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AN EVALUATION OF  
ACCIDENTAL WATER-REACTIONS WITH LITHIUM  
COMPOUNDS IN FUSION REACTOR BLANKETS

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AN EVALUATION OF ACCIDENTAL WATER-REACTIONS  
WITH LITHIUM COMPOUNDS IN FUSION REACTOR BLANKETS

ABSTRACT

Efforts to mitigate potential problems of lithium-based blankets for fusion reactors include the use of lithium compounds for breeding purposes. This report investigates the safety aspects of these alloys relative to the use of pure lithium in a water-cooled blanket. Included in the study is a modification of the LITFIRE computer code to predict the thermal response of an internal blanket breeder-water interaction.

For the problem analyzed, results indicate that some of the lithium-lead alloys may pose safety problems approximate to those associated with the use of liquid lithium.  $\text{Li}_2\text{O}$  is shown to be significantly safer than liquid lithium, while results using  $\text{LiAl}$  are similar to those of the lithium-lead alloys.

In addition, the study provides an overview of this safety question, signaling areas that require further development.

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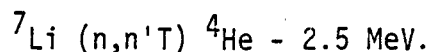
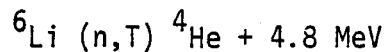
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## CHAPTER 1. INTRODUCTION

Advancements in plasma physics research, together with a growing concern for the risks of energy production in the public sector, has led to an increasing number of detailed fusion safety studies. Topics, including routine and accidental releases of tritium, activation of structural material by neutron bombardment, and the consequences of lithium fires, are currently under various degrees of investigation. The findings of these studies are incorporated in subsequent fusion reactor designs, answering some questions and creating still more.

This work is the product of a research program whose objective is to minimize the potential problems of a lithium-based blanket for fusion reactors. Such a blanket is practically forced upon us by the choice of a D-T fuel mixture for first generation fusion power plants [1]. The needed tritium is bred via the reactions:



Initially, natural lithium (92.58%  ${}^7\text{Li}$ , the rest  ${}^6\text{Li}$ ), a liquid at operating blanket temperatures, was the primary candidate for blanket breeder and/or coolant materials, due to its excellent breeding and heat transfer qualities, effectiveness in neutron moderation and relatively low pumping power need as compared to other liquid metals [2]. However, with time and study, serious disadvantages in the use of liquid lithium emerged.

Pure lithium is highly reactive with air, water and concrete; all materials that will be in abundant supply in the reactor environment. Experimentation at the Hanford Engineering Development Laboratory (HEDL) and computer modelling studies at MIT using the computer code LITFIRE (to be discussed in more detail later in this report) indicate that temperatures and pressures in the reactor containment area, in the event of a sizable lithium spill, can attain critically high values [3]. Figure 1.1 shows such a possibility. Such an event could provide a pathway for release of tritium or structural activation products, providing a hazard to plant personnel or the outside world.

This problem and others, including corrosion, difficulties in tritium recovery, and magnetohydrodynamic instabilities [4], have led designers to consider alternative materials for fusion blankets. Among such considerations are lithium-lead alloys.

This report will provide a preliminary analysis of lithium-lead alloys for use as breeding materials from the safety point of view. While it is thought that these materials provide less of a hazard than the use of liquid lithium, little has been demonstrated. Thus, there is the need to formulate some framework for a comparison.

Before actual calculations can be made, a basis must be established. The NUWMAK reactor design by the University of Wisconsin (1978) was chosen for this purpose, due to its use of  $\text{Li}_{62}\text{Pb}_{38}$  eutectic as the tritium breeder. The primary hazard here involves interaction between the lithium-lead alloy breeder and the boiling water coolant, inside the blanket. Specifics of this design are further discussed in Chapter 2.

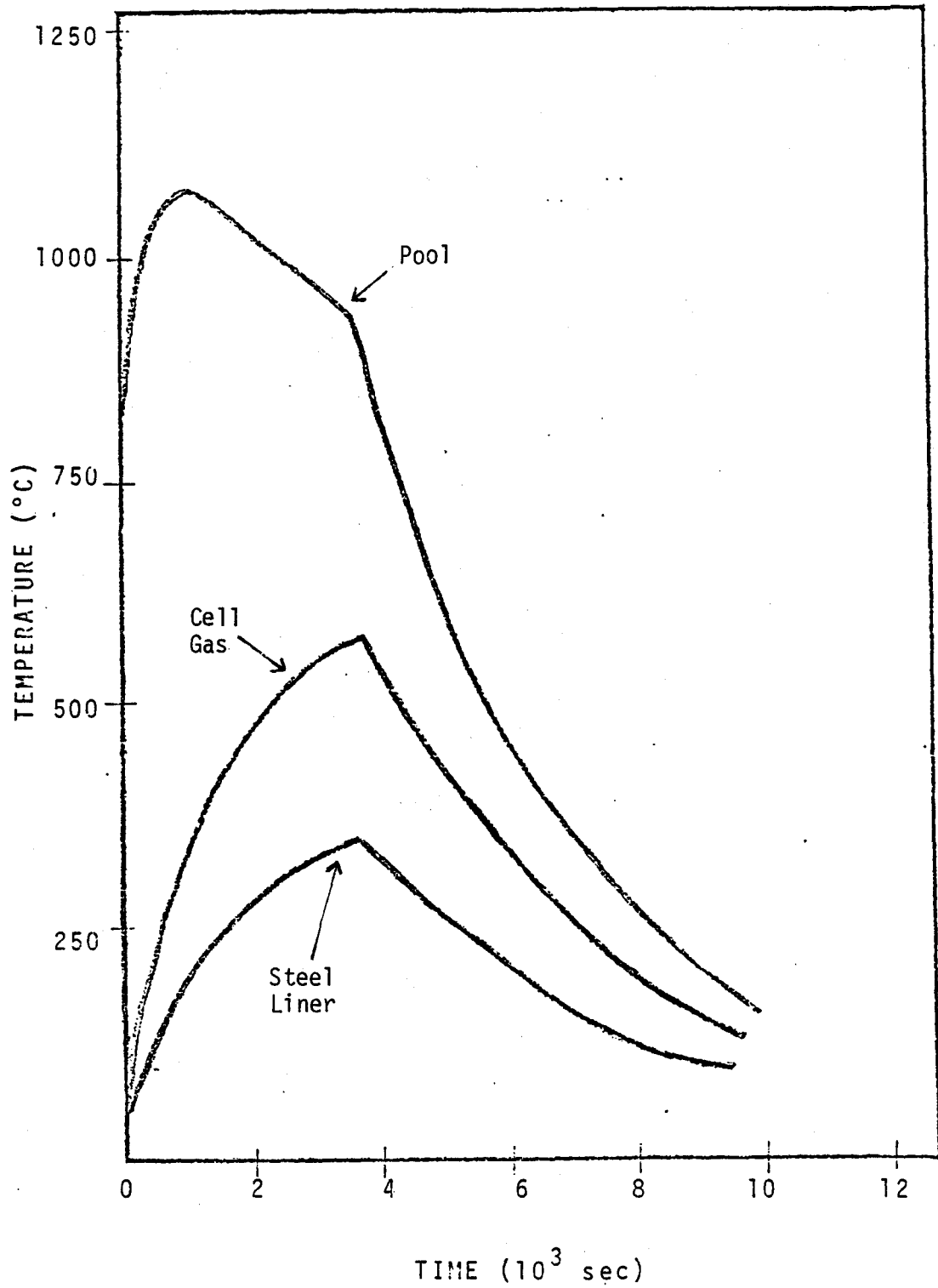


Figure 1.1 LITFIRE predictions for consequences of lithium spill in UWMAK III containment (Reference 3).

Using this basis, two separate studies are performed. The first is a static calculation: the breeder and coolant are allowed to interact immediately and the subsequent equilibrium final temperature of the blanket materials is determined. This is presented in Chapter 3. The second study is a dynamic calculation, using LITFIRE, of the temperature histories at various points in the blanket, if some accident allows breeder and coolant to come into contact. This is presented in Chapter 4. It should be stressed that in both studies, the values obtained are not sufficient evidence in themselves. Rather, these values must be compared with similar calculations employing the use of pure lithium. In this way, a measure of the relative hazards of the alternate breeders can be assessed.

## CHAPTER 2. BLANKET DESIGN BASIS DESCRIPTION

### 2.1 Introduction

NUWMAK, a conceptual thermonuclear reactor designed by the Fusion Engineering Program of the University of Wisconsin in March 1979, is one of a number of second generation studies aimed at maximizing the strengths of fusion while minimizing the weaknesses. This work builds upon the findings of a number of first generation designs aimed at identifying the important problems of fusion power.

The design philosophy of this study was to search for an "end product that has the potential to be reliable, maintainable, environmentally acceptable, and reasonably economic [4]." To do this, a number of changes were made to the preceding reactor concept, UWMAK III, including: an increase in the magnetic field to increase power density, a simplification of design to facilitate maintenance (as well as eliminate large cost items), the selection of structural materials to minimize resource requirements and costs, and a change in blanket breeder and coolant materials to reduce thermal fatigue and thereby increase reliability. The resulting structure is shown in Figures 2.1 and 2.2

The new elements in blanket breeder and coolant materials are of particular interest to those concerned with fusion safety studies. Utilized in NUWMAK are: (a)  $\text{Li}_{62}\text{Pb}_{38}$  eutectic for the breeding material, used because its melting point is very near the blanket operational temperature and thus, the latent heat of melting can provide energy storage, and (b) boiling water for the coolant, the "perfect choice," discarded previously with the presence of pure lithium as the breeder.

CROSS-SECTIONAL VIEW OF  
NUWMAK

Figure VIII-A-1

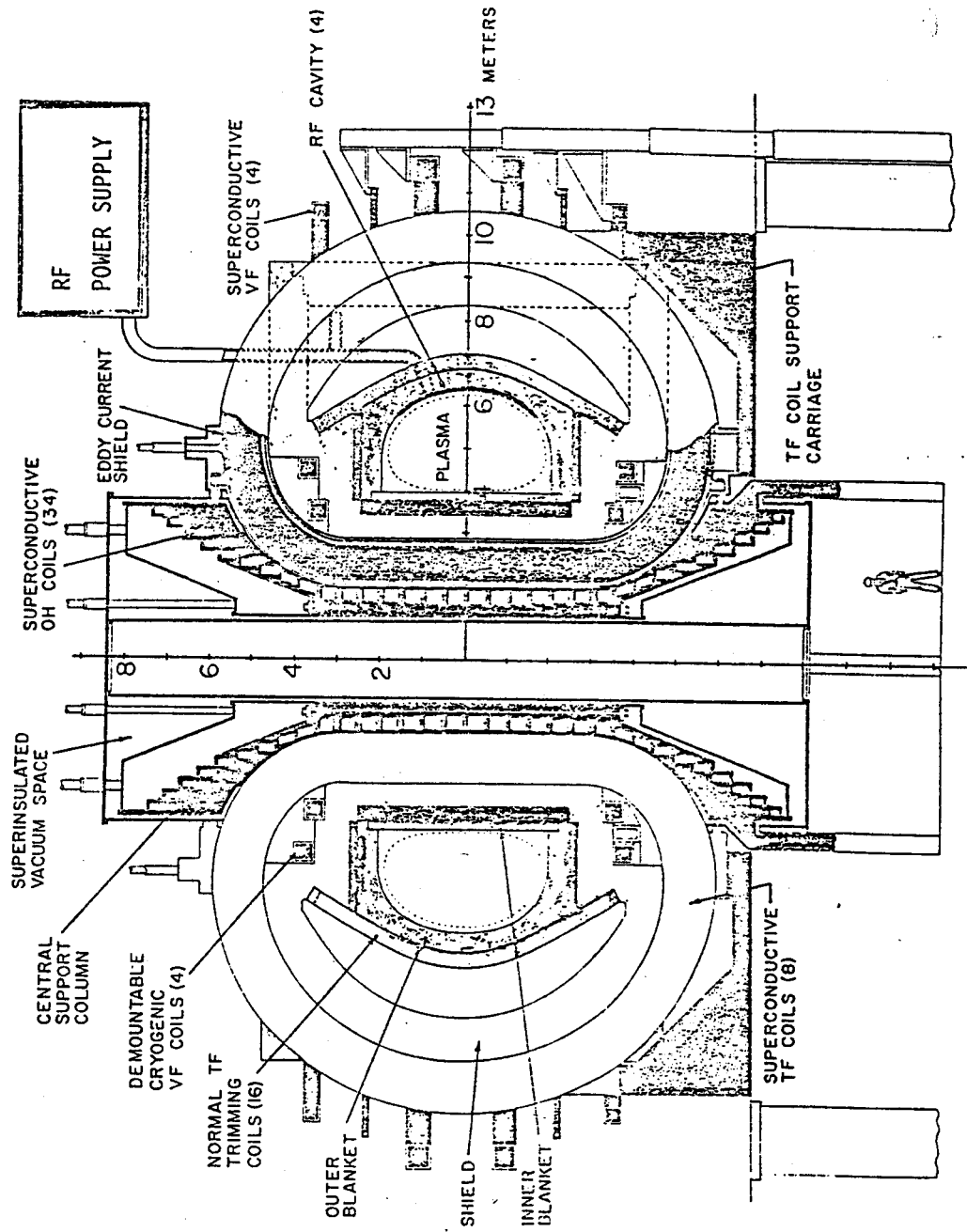


Figure 2.1 Cross-sectional View of NUWMAK (Reference 4).

# TOP VIEW OF NUWMAK

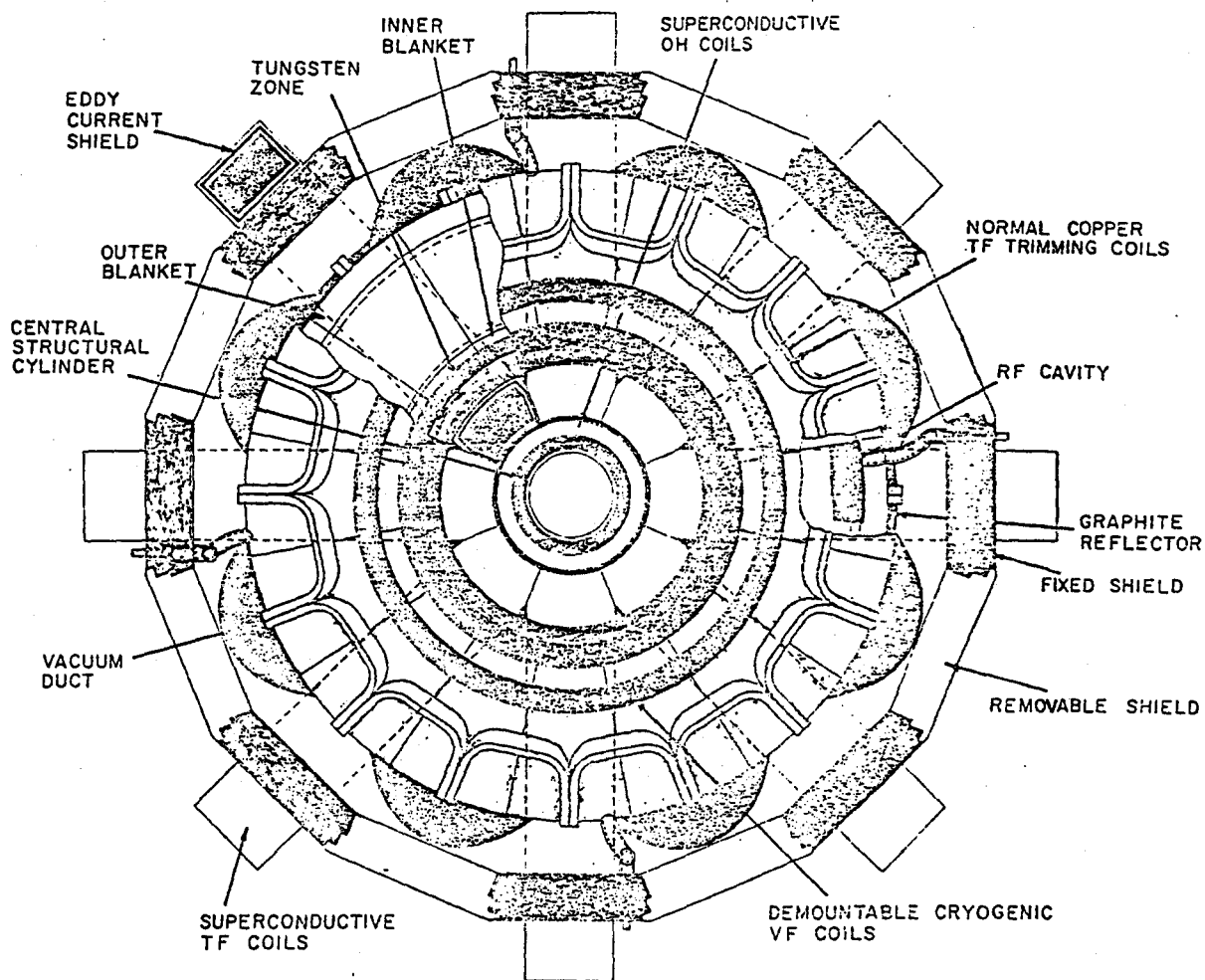


Figure 2.2  
(Reference 4)



A preliminary survey of the hazards of lithium-lead alloys indicates that interaction with water is by far the more severe problem, as these materials are relatively inert in air. NUWMAK, in addition to its use of  $\text{Li}_{62}\text{Pb}_{38}$ , provides an opportunity for the breeder and coolant to come into contact, specifically a breach in the cooling system inside the blanket. Thus, NUWMAK is the logical first choice for a basis for an investigation of the relative safety of the lithium-lead alloys.

## 2.2 Breeding Materials

### 2.2.1 Lithium-lead alloys

The lithium compound selected as the tritium breeding material must satisfy many requirements. It must have desirable neutronic and irradiation characteristics, chemical stability at blanket operating temperatures, and be compatible with other blanket materials. More importantly, the compound must breed and release tritium at sufficient rates to fuel the reactor, yet limit the tritium inventory in the blanket to reasonable levels.

Lithium-lead compounds are interesting materials. Figure 2.3 shows the phase diagram of a Li-Pb two component mixture. However, beyond  $\text{Li}_7\text{Pb}_2$ , considered the most attractive lithium-lead alloy for breeding purposes, little else on the subject of Li-Pb physical properties is certain. An accumulation of data relevant to this study through a literature search and "data synthesis" is presented in Appendix A.

Two neutronic characteristics of the lithium-leads, breeding capability and long-lived activation products, have been studied. In the latter only  $^{205}\text{Pb}$  presents any problem in the long term unless significant amounts of impurities exist. This is not expected to be serious [4]. Breeding

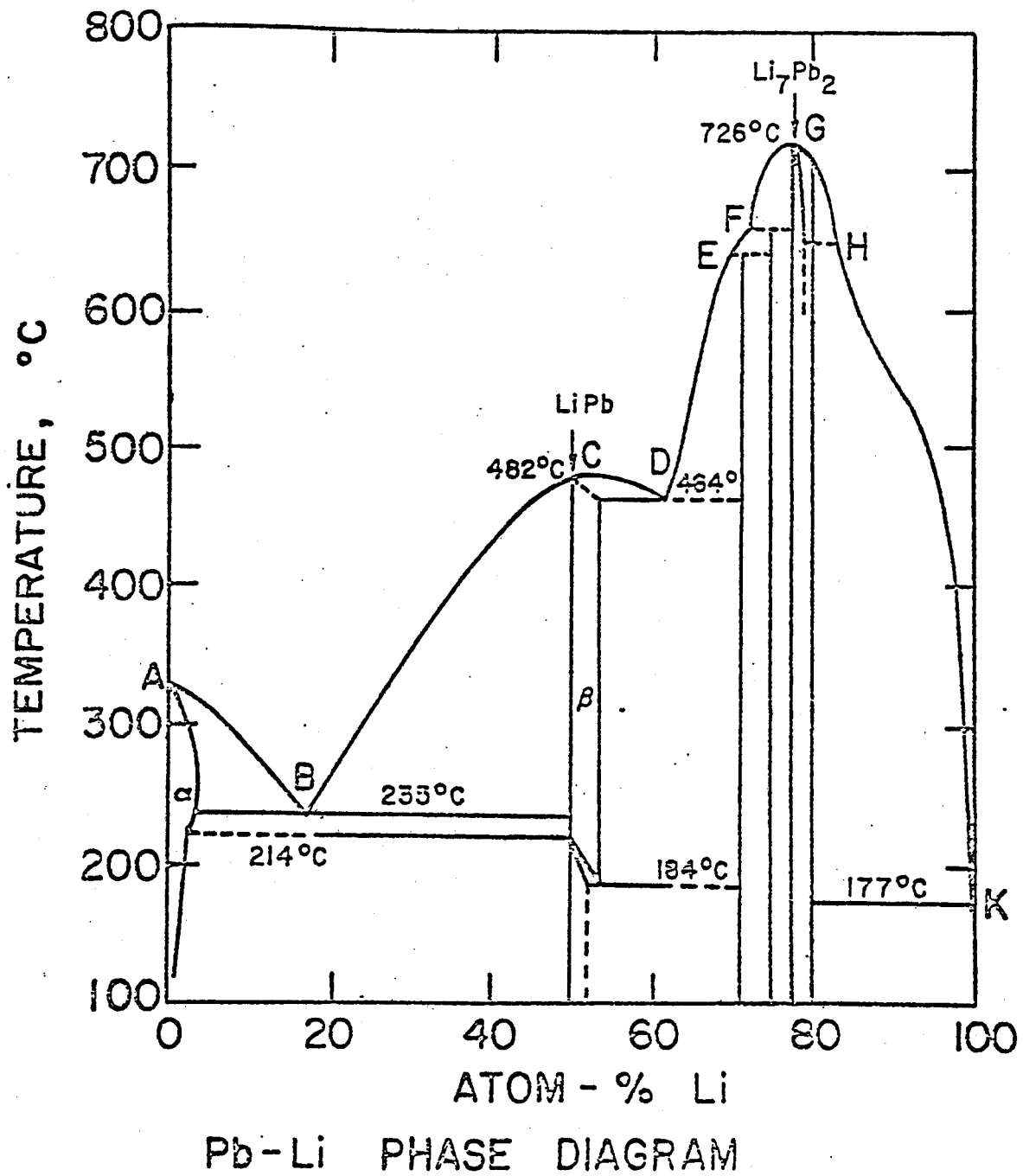


Figure 2.3  
(Reference 4)

capability depends on the amount of lead present.

$\text{Li}_7\text{Pb}_2$  has been examined in detail and exhibits an excellent breeding property. This is due to the presence of lead, which acts as a neutron multiplier. Figure 2.4 shows the effect of lithium concentration in the lithium-lead breeder on the total breeding ratio. The total bulk shield thickness required to protect toroidal field coils is shown for reference. It is evident that a reduction of the lithium concentration will cause a substantial loss of fuel multiplication. However, the reduction of lithium also tends to enhance magnet protection by virtue of more effective nuclear radiation shielding by the added lead [5].

A diffusion study by Wiswall [6] shows that the solubility of tritium in Li-Pb is much lower than that in pure lithium, as the activity of lithium is very low due to the presence of lead. Thus, the tritium inventories can be much smaller, tritium diffusivities relatively higher, and tritium recovery much easier. Specifically, Fig. 2.5 shows that  $\text{Li}_7\text{Pb}_2$  has the lowest inventory of any of a number of proposed breeders. A problem here could be the fact that  $\text{Li}_7\text{Pb}_2$  becomes a "chunk" at high temperature. This would increase the diffusion path of tritium and make recovery difficult [4].

A more serious problem of the lithium-leads involves their compatibility with the blanket environment. All react to some extent with water. Table 2.1 shows the results of experimentation to investigate this at Argonne National Laboratory. It can be seen that Li-Pb alloys can react vigorously with water, more so at elevated temperatures. However, a significant result is that  $\text{Li}_{17}\text{Pb}_{83}$  exhibited only moderate reaction with water. Also, insufficient hydrogen was evolved by the alloy reactions to attain ignition conditions, unlike the case with liquid lithium.

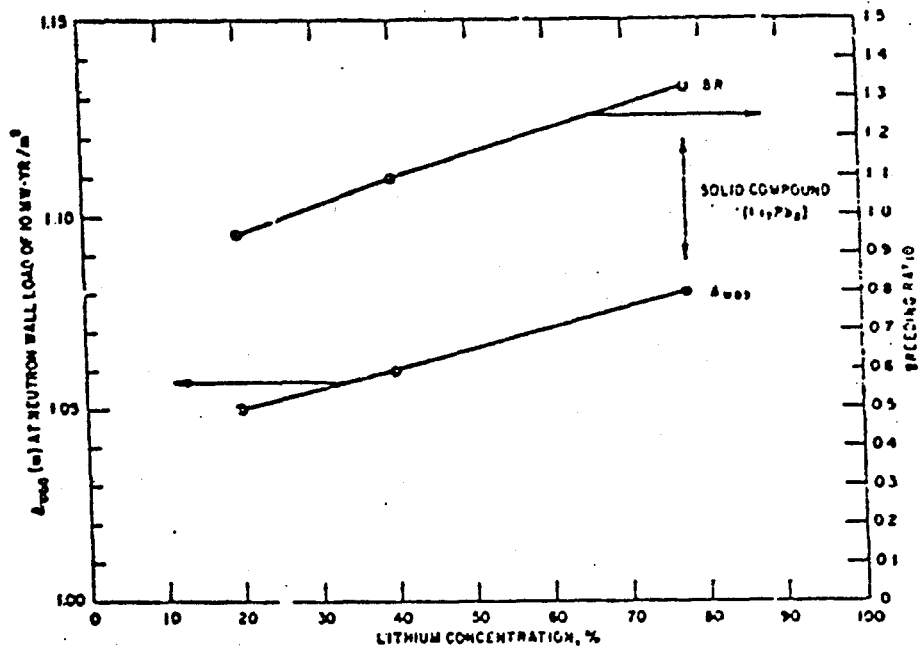


Figure 2.4 Effects of lithium concentration in a lithium-lead breeder on shielding requirement and tritium breeding (Reference 5).

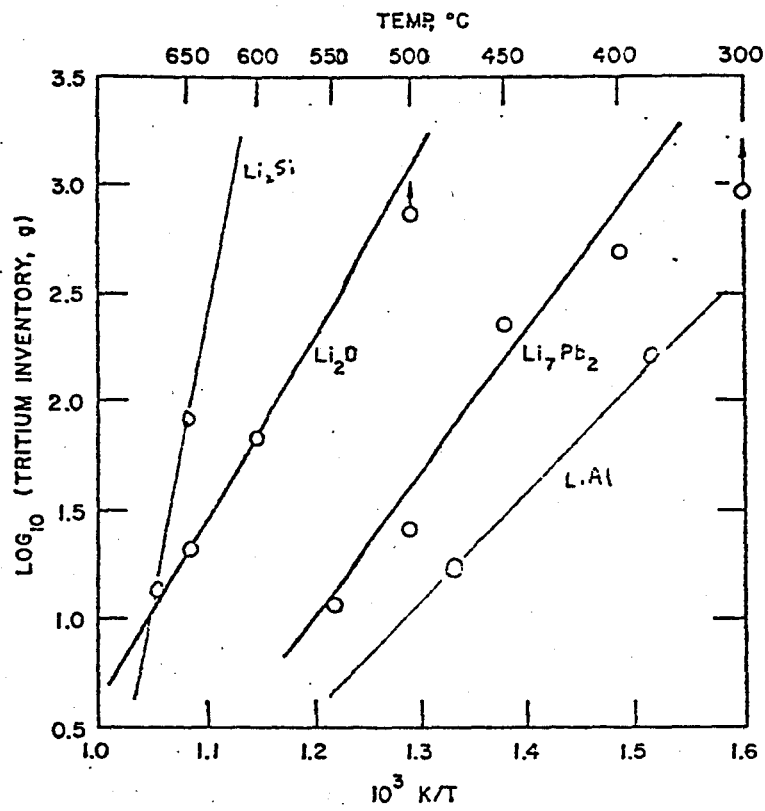


Figure 2.5 Estimated tritium inventory in alternative breeder blankets for a 3000 MW<sub>th</sub> reactor (Reference 9).

TABLE 2.1  
 Reactions of Li-Pb Alloys and Lithium  
 with Water

Case	Sample			Water Temp/°K	Reaction
	Composition	State	Temp/°K		
1	Li <sub>7</sub> Pb <sub>2</sub>	s	773	298	Modest
2	Li <sub>7</sub> Pb <sub>2</sub>	s	773	369	Vigorous
3	Li <sub>7</sub> Pb <sub>2</sub>	s	873	368	Vigorous
4	Li <sub>7</sub> Pb <sub>2</sub>	ℓ	1103	368	Very Vigorous
5	Li <sub>0.62</sub> Pb <sub>0.38</sub>	ℓ	773	368	Vigorous
6	Li <sub>0.17</sub> Pb <sub>0.83</sub>	ℓ	773	368	Very modest
7	Li	ℓ	773	368	H <sub>2</sub> Detonation
8	Li <sup>a</sup>	ℓ	773	368	Detonation

<sup>a</sup> Injected under water

(Reference 7)

In all reactions, LiOH (melting point at 470 °C) is formed. Liquid LiOH is an extremely corrosive substance and would degrade the integrity of the activated structural materials [7]. Fortunately, Li-Pb is relatively inert in air. It was reported [8] that "LiPb (50-50 mixture) resembles Pb in every respect except density. LiPb would not ignite, even when exposed to the flame of a gas-air torch." Therefore, though a Li-Pb - H<sub>2</sub>O reaction could be very serious, it is not expected to be as severe as an accident involving pure lithium. Table 2.2 provides a summary of the advantages and disadvantages of the lithium-lead alloys.

### 2.2.2 Alternative Breeders

For completeness, LiAl and Li<sub>2</sub>O, also candidates for the tritium breeding material, will be analyzed with regard to safety in this study. Other strong candidates, specifically Li<sub>2</sub>SiO<sub>3</sub> and LiAlO<sub>2</sub>, have been ignored in this study since they have no appreciable reaction with water.

LiAl is in many ways akin to Li<sub>7</sub>Pb<sub>2</sub>, such as a similarity in reactivity with water. However, the latter material is preferred by designers due to a superior tritium breeding capability. This is because there is a lower lithium-atom density in LiAl and no neutron multiplier, with the absence of Pb. Tritium extraction characteristics are also poorer than that of Li<sub>7</sub>Pb<sub>2</sub> [9]. The primary activation product is <sup>26</sup>Al, more of a problem than <sup>205</sup>Pb. Physical properties of this breeder are also unexplored and are discussed in Appendix A. The phase diagram is shown in Fig. 2.6.

Li<sub>2</sub>O has a marked advantage over the lithium-lead alloys in the matter of reaction with water. Because it is in oxide form, this compound does not evolve hydrogen upon reaction and produces less heat [9]. It is

TABLE 2.2

Summary of Favorable and Unfavorable Features of  
Lithium-Lead Breeders

Lithium-Lead Alloys

Advantages

1. High breeding ratio attainable
2. Probably less reactive with water than liquid Li
3. Tritium recovery appears feasible with low-pressure helium
4. Lead helps shield magnets

Disadvantages

1. Poor technology base: high degree of uncertainty in properties
2. Reactive with water coolant
3. High blanket weight
4. Uncertain radiation damage effects
5. Uncertain tritium release mechanism
6. Requires blanket changeout during reactor life
7. Activation product:  $^{205}\text{Pb}$



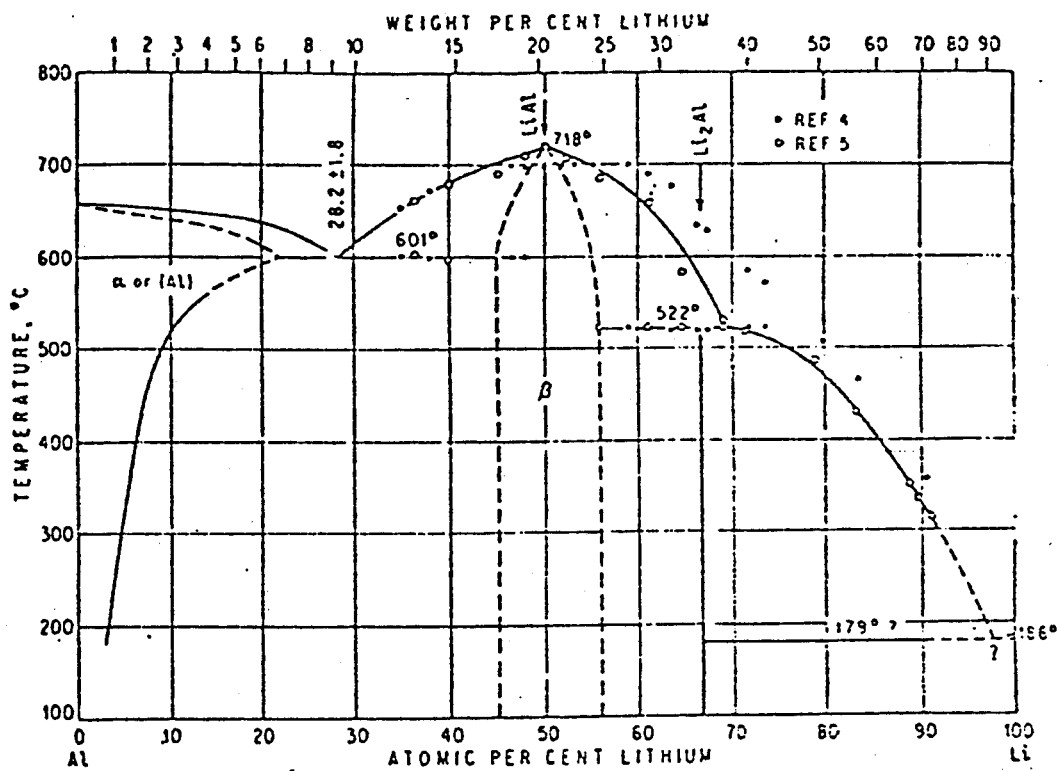


Figure 2.6 Phase Diagram for LiAl System.  
(Reference 9)

therefore expected that the use of this breeder will not pose a major safety problem. However,  $\text{Li}_2\text{O}$  has fallen into disfavor because it has a high lithium-atom density. This, combined with a poor diffusion rate, leads to excessive tritium inventories. Physical properties of this breeder are also discussed in Appendix A.

### 2.3 Coolant

Many factors affect the choice of coolant. Unique in power production to fusion is the interrupted burn cycle of the plasma. This produces the problem of thermal fatigue in the first wall and blanket, caused by the fluctuating temperature of these structures with the plasma burn cycle. The temperature change is a combination of three effects:

1. Coolant temperatures rise,  $T_{c,out} - T_{c,in}$
2. Film temperature drop,  $T_{wall} - T_c (=Q/h)$
3. Temperature difference across the first wall,  $\Delta T = Q \chi/k$  [4].

While the third effect depends on structural materials, the first two can be greatly reduced by choice of the proper coolant, one which has a small coolant temperature rise that simultaneously provides a large heat transfer coefficient. This describes a boiling liquid and the first logical choice is boiling water.

A considerable technology has been developed through the years for the use of water as a coolant in energy production. There exist many advantages. Water is an excellent heat-transfer fluid, costs little and is readily available. It is easy to pump and is non-corrosive with conventional structural materials.

It is interesting to note, however, that up to this point, few designers have considered water for the primary coolant. There exist a number of concerns and questions including neutronics, tritium, and safety considerations. In addition, the use of a boiling water or steam coolant will require high pressure containment. The NUWMAK design calls for cooling water at 300 °C and 8.6 MPa (1250 psi). This poses additional design and safety problems.

The safety concerns of a water-cooled blanket have been discussed. It should be noted that this problem effectively prohibited the use of water as a coolant until alternative breeders to lithium were suggested. Even so, current designs using water stress the use of strong cladding materials for coolant channels.

High-integrity cladding is also the prescription to minimize tritium diffusion into the cooling water. Tritiated water is a safety hazard and recovery of the tritium is difficult and expensive. However, recent studies using permeation rates for stainless steel cooling tubes show tritium losses could be less and 1 Ci/day, assuming the formation of oxide films inside the tubes [9]. Irregardless, it is obvious that the coolant loop cannot be used for tritium recovery, necessitating some recirculation of the breeder.

The necessity of avoiding contact between breeding materials and coolant tends inherently, to increase structural material content in the blanket. From a neutronics point of view, this increase tends to degrade the tritium breeding ability, due to increased parasitic neutron absorption. However, the strong neutron slowing-down power of water improves breeding performance by increasing the  ${}^6\text{Li} (n,T) {}^4\text{He}$  reaction rate for low energy neutrons. This decreases parasitic absorption by

the structural materials [5]. Therefore, proper design and choice of materials can leave the tritium breeding capability of a water-cooled blanket virtually unchanged.

Figure 2.7 shows this phenomenon for various breeders, with 316 stainless steel used as structural material. It is important to note that the addition of water significantly improves the breeding ratio in the  $\text{Li}_7\text{Pb}_2$ , more so than the other breeders. This is due to reduced parasitic absorption in lead as well as the stainless steel.

Table 2.3 summarizes the advantages and disadvantages of the water-cooled blanket concept. Chief among the assets is the use of available technology in its construction. The major liabilities appear to be the safety problem and limited choices in compatible breeding and structural materials. Further study in both areas is necessary before a final decision can be made.

## 2.4 NUWMAK Blanket Design

### 2.4.1 Structural Materials

Many structural materials have been considered for a water-cooled blanket design, including: austenitic stainless steel, high nickel alloys and selected titanium, vanadium and niobium alloys [9]. Table 2.4 summarizes an assessment of these candidates with regard to properties associated with the blanket environment.

One of the liabilities of the water-cooled design is apparent. The vanadium and niobium materials, which respond well to neutron bombardment, are eliminated due to water corrosion problems. Also noted is a general lack of data regarding the compatibility of these structural materials with the lithium-lead alloys. Since decomposition of these alloys is not

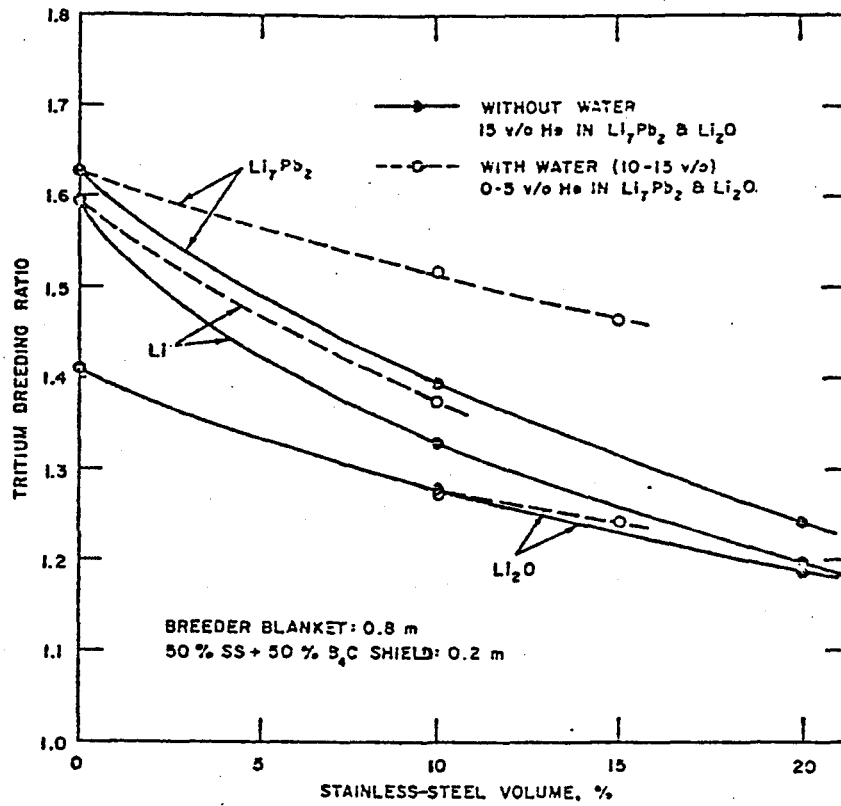


Figure 2.7 Impact of Structural Material Content (316 SS) on Tritium Breeding (Reference 6).

TABLE 2.3

Summary of Favorable and Unfavorable Features of  
the Water-Cooled Blanket Concept

Water Coolant

Advantages

Disadvantages

- |  |   |
|--|---|
| 1. Excellent heat-transfer fluid                         | 1. Highly reactive with candidate breeding materials          |
| 2. Well-developed technology base                        | 2. Reaction product (LiOH) is very corrosive                  |
| 3. Low cost and readily available                        | 3. Requires high-pressure containment                         |
| 4. Relatively low temperature ( $\sim 320$ °C) operation | 4. Cannot be used for tritium recovery                        |
| 5. Compatible with conventional structural materials     | 5. Expensive to remove tritium from H <sub>2</sub> O (safety) |
| 6. Low pumping power need                                | 6. Water tends to be a sink for tritium                       |
| 7. Enhances tritium production                           |   |
| 8. Liquid at room temperature                            | 7. Nb and V, candidate structure materials are incompatible   |

TABLE 2.4

Summary of Structural Material Assessment for the  
Water-Cooled Blanket Concept

Property Requirement	Rating*				
	Fe	Ni	Ti	V	Nb
Bulk Radiation Effects	2	2	?	1	1
Compatibility with H <sub>2</sub> O	1	1	1	4	4
Compatibility with Liquid Li	3	5	3	1	1
Compatibility with Solid Li <sub>2</sub> O and Li <sub>7</sub> Pb <sub>2</sub>	3	3	3	3	3
Compatibility with H(DT) Environment	1	1	3	1	1

\* Rating numbers defined as follows:

1. Compares favorably with other candidate structural materials.
2. Limits operating life but probably acceptable under certain conditions.
3. Little data available but may be a limiting factor.
4. Probably not viable for conditions of interest.

desirable, this question should be studied.

The NUWMAK design utilizes Ti-6Al-4V alloy for the first wall and coolant tube material due to its high strength-to-weight-ratio, good fatigue resistance, fabricability, low long term residual activity and well established industry [4]. Physical properties of this alloy are shown in Table 2.5. The NUWMAK shield is more conventional, primarily  $B_4C$ .

#### 2.4.2 Mechanical Design

The blanket of NUWMAK is shown in Fig. 2.8. The blanket structure is Ti-4Al-4V which operates at a temperature of approximately 350 °C. The coolant is boiling water at 300 °C and 1250 psi. The breeder is  $Li_{62}Pb_{38}$  eutectic, operating at approximately 400 °C. The design life for each blanket module is two years.

The blanket is divided into eight modules in the reactor. Each module is fed and discharged coolant and breeding materials separately. There are two blanket units in each module; the inner blanket near the machine axis and the outer blanket, as seen in Fig. 2.8. These two units are completely separate from each other.

The first wall consists of a continuous bank of tubes running in the vertical direction. Beyond this, the blanket is cooled with rows of vertical tubes on a triangular pitch. The spacing between rows of tubes is progressively increased towards the back of the blanket to account for the radially decreasing nuclear heating [4]. Radial struts are spaced at 20 cm intervals, reinforcing the first wall against the hydrostatic pressure of the breeding material, which fills the space between the coolant tubes.



TABLE 2.5

Physical Properties of Ti-6-4

Atomic Weight	45.9
Melting Point	1668 °C
Mass Density	4.4 g/cm <sup>3</sup>
Yield Strength	530 MPa
Modulus of Elasticity	85 GPa
Yield-to Weight Ratio	120 N-m/g
Thermal Condcutivity	.12 W/cm-K
Coefficient of Thermal Expansion	10 x 10 <sup>-6</sup> /°C
Heat Capacity	668.8 J/kg-K

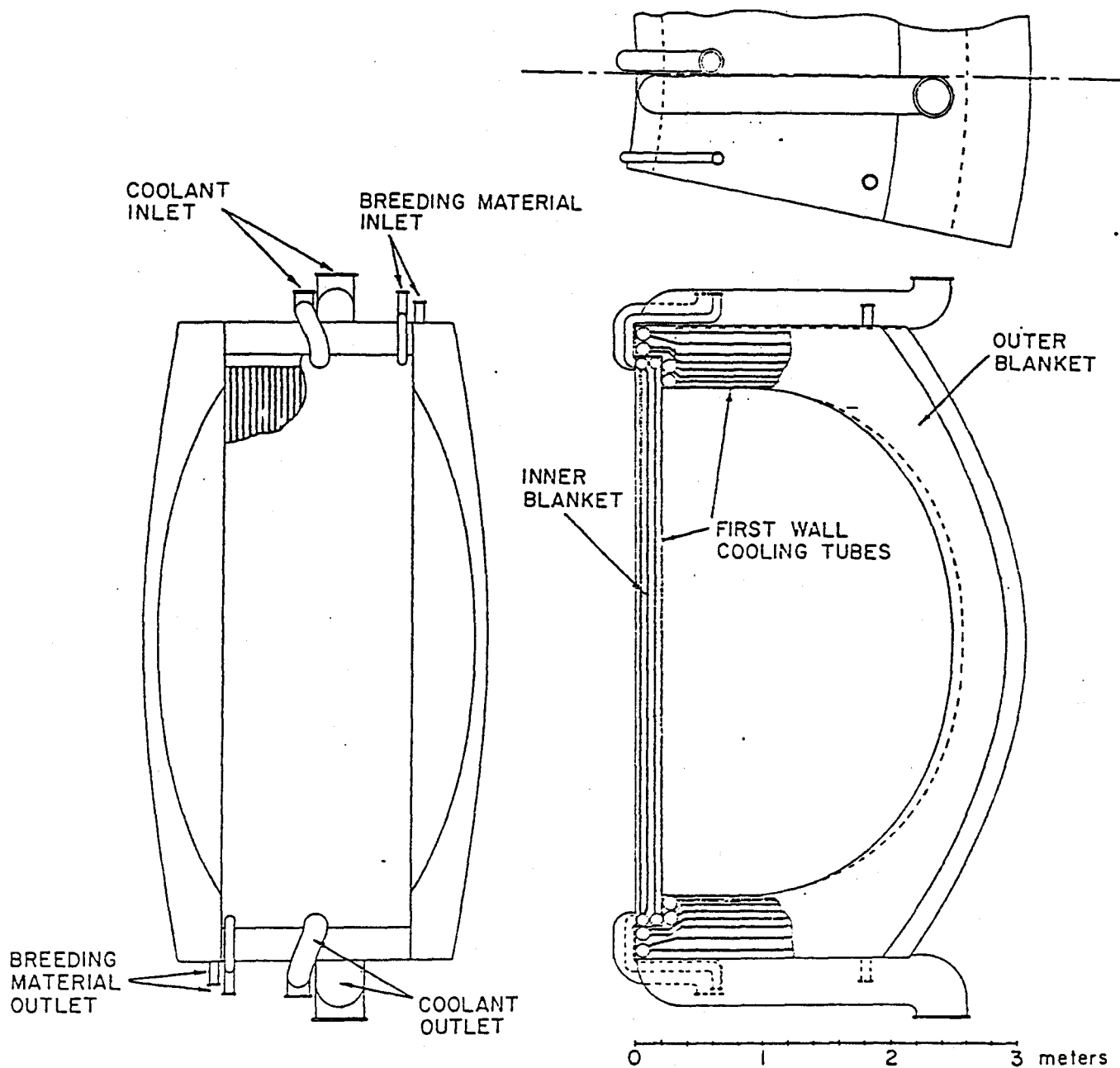


Figure 2.8 Cross-Sectional View of Blanket (Reference 4).

At the blanket's edge is a thin graphite reflector. Beyond this is a shield to protect the cryogenic magnet coils. The shield is primarily  $B_4C$ , operating at approximately 150 °C. Figure 2.9 shows a schematic diagram of this system.

#### 2.4.3 Summary of Important Parameters

The major features of the NUWMAK design are given in Table 2.6. In addition, important blanket parameters pertinent to this study are given in Table 2.7. These values are used where appropriate in subsequent calculations.

## SCHEMATIC OF THE BLANKET AND SHIELD FOR NUWMAK

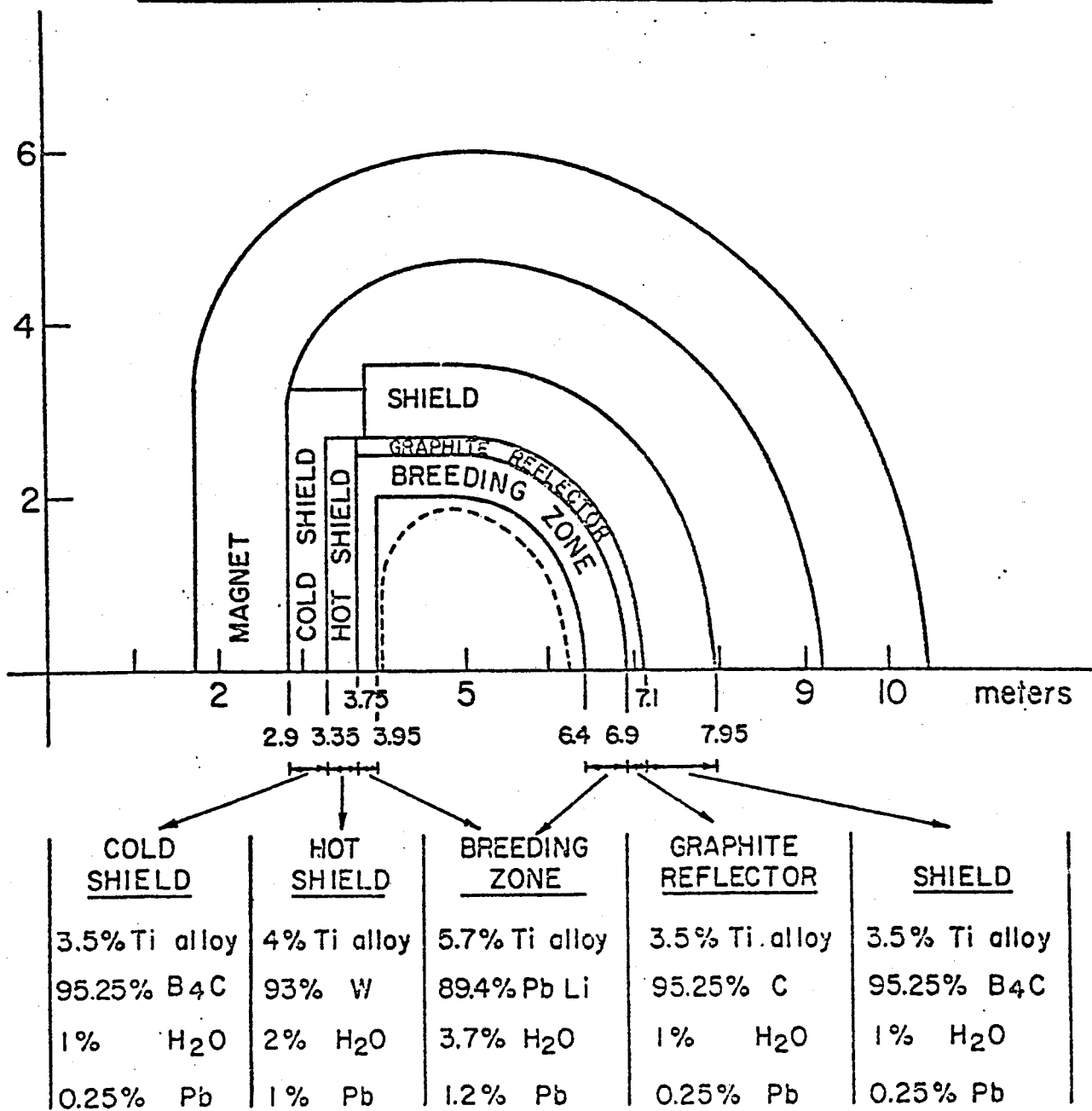


Figure 2.9  
(Reference 4)

TABLE 2.6

Major Features of NUWMAK Design

Power

Total Thermal Power	2283 MW <sub>th</sub>
Net Electric Power	660 MW <sub>e</sub>

Plasma

Major Radius	5.13 m
Minor Radius	1.13 m
Plasma Height to Width Ratio (b/a)	1.64
Plasma Current	7.2 MA
Toroidal Beta	6%
$n_e \tau_E$	$2 \times 10^{14}$ cm <sup>-3</sup> -sec
q(a)	2.64

Magnet

On-Axis Toroidal Field	6.05 Tesla
Toroidal Field at NbTi Conductor	11.5 Tesla
Stabilizer	Aluminum
Number of Toroidal Field Coils	8
Number of Cu Trim Coils	16

Blanket

Structural Material	Titanium Alloy
Coolant	Boiling Water
Breeding Material	Li <sub>62</sub> Pb <sub>38</sub>
Average Neutron Wall Loading	4.34 MW/m <sup>2</sup>

TABLE 2.7

Summary of Important Blanket Parameters

Plasma Burn Time	225 sec
Plasma Down Time	20 sec
Coolant Temperature	300 °C
Coolant Pressure	8.6 MPa
Total Coolant Flow Rate	1500 kg/sec
Total Coolant Tube Surface Area	4350 m <sup>2</sup>
Heat Transfer Coefficient of Boiling Water	20000 Btu/hr-ft <sup>2</sup> - °F
Coolant Tube OD	1.3 cm
Coolant Tube ID	1.0 cm
N. Tubes in Outer Blanket Module	475
Pitch Length	12 cm
Space for Breeder in Outside Blanket Module	17.72 m <sup>3</sup>
Breeder Temperature	400 °C
Shield Temperature	150 °C



## CHAPTER 3. EQUILIBRIUM $T_f$ CALCULATION

### 3.1 Introduction

Lithium-lead alloys are considered less of a safety hazard due to the presence of lead, which is thought to slow down the water reaction, decrease the heat of reaction and help absorb what heat is released. However, a number of physical properties are altered with the addition of lead. Since most of these properties have direct bearing on an interaction with water, the consequences of such an interaction are not directly predictable.

For this reason, a preliminary analysis of the Li-Pb - H<sub>2</sub>O reaction is performed using a static calculation. In this case, the breeder inside one blanket module is allowed to interact completely with varying amounts of the water available to that module. Assuming the heat of reaction is contained within the blanket, the equilibrium temperature of the reaction products, unreacted breeder and blanket structural materials is then determined.

Such a scenario is unrealistic, but this calculation is important for two reasons. First, it serves as a reference for further study. Second, with its assumptions, such a calculation may indicate the maximum attainable blanket temperature in a particular module in the case of an internal blanket water interaction.

### 3.2 Assumptions and Methodology

The outer blanket section of an individual module is chosen for consideration. The inner blanket section contains only a nominal amount of breeder and the consequences of an accident in that section do not



appear as severe. Data from the NUWMAK design (Table 7.H.2) indicates that an outer blanket module contains 38.4 tonnes of titanium structural material, 106.0 tonnes of graphite and 17.7 m<sup>3</sup> of space to contain the breeder. Therefore, the amount of breeder present can be determined with knowledge of the density.

The initial temperature of breeder and graphite is 400 °C. The structural materials are at a temperature of 350 °C and the coolant is at 300 °C and 1250 psi. The reaction between breeder and coolant is assumed to be immediate and complete at 400 °C, the heat of reaction helping to raise the water temperature to that point. The heat of reaction can be determined using:

$$\Delta H_r = \Delta H_{25}^\circ + \Sigma \Delta H_{\text{prod}} - \Sigma \Delta H_{\text{react}}, \text{ cal/g breeder} \quad (3.1)$$

where  $\Delta H_{25}^\circ$  is the standard heat of hydrolysis at 25 °C and  $\Delta H_{\text{prod}}$  and  $\Delta H_{\text{react}}$  are the enthalpy changes of reaction products and reactants, respectively, as they are heated from 25 °C to 400 °C.

The amount of coolant water available to the outer blanket module can be determined by analysis of NUWMAK's steam generating unit. In this respect, NUWMAK is very much like a fission boiling water reactor [4]. Examination of the Dresden BWR reveals that the total coolant volume in the 3411 MW<sub>th</sub> plant's cooling system is 11,695 ft<sup>3</sup> [10]. Scaling this down to NUWMAK's 2283 MW<sub>th</sub> output and assuming the average density of water in the coolant loop to be 62.37 lb/ft<sup>3</sup> (an overestimate), it can be shown that approximately 15,260 pounds of water are available to interact with the breeder in one module.

It is assumed that a fixed percentage of this cooling water interacts with the breeder. Thereafter, no loss of heat is allowed from the blanket. The resulting final equilibrium temperature can be calculated using the expression

$$T_f = T_o + \frac{Q_R}{(M_s \bar{C}_s + M_b \bar{C}_b + \sum M_{Ri} \bar{C}_{Ri})} \quad (3.2)$$

where  $T_f$  = final equilibrium blanket temperature  
 $T_o$  = initial blanket temperature  
 $Q_R$  = reduced heat of reaction  
 $M_s$  = structural mass  
 $M_b$  = remaining breeder mass after reaction  
 $M_R$  = reaction product mass after reaction  
 $\bar{C}_i$  = mean specific heat for each component

Reaction products include hydrogen gas, LiOH and the alloy element.

A proper evaluation of the  $M_i \bar{C}_i$  terms in the above equation varies with each component. For example, LiOH is evaluated above its melting point as

$$M_{LiOH} \bar{C}_{LiOH} = \frac{M_{LiOH} [\bar{C}_s (T_{melt} - T_o) + \Delta H_{melt} + \bar{C}_L (T_f - T_{melt})]}{T_f - T_o} \quad (3.3)$$

where  $\bar{C}_s$  = mean solid specific heat of LiOH  
 $\bar{C}_L$  = mean liquid specific heat of LiOH at 470 °C  
 $\Delta H_{melt}$  = heat of melting for LiOH at 470 °C  
 $T_{melt}$  = melting point of LiOH (470 °C)

Similar expressions can be written for the other components.

The reduced heat of reaction can be written as

$$Q_R = xM_C [a_0 \Delta H_R - \bar{C}_C (T_0 - T_C)] - M_{Ti} \bar{C}_{Ti} (T_0 - T_{Ti}), \quad (3.4)$$

where

$M_C$  = mass of total available coolant

$M_{Ti}$  = mass of titanium structural material

$\bar{C}_C$  = mean specific heat of coolant

$\bar{C}_{Ti}$  = mean specific heat of titanium structural material

$T_C$  = coolant temperature

$T_{Ti}$  = titanium structural material temperature

$x$  = fraction of available coolant reacting

$a_0$  = reaction stoichiometric combination constant

This is done to raise the coolant and titanium alloy structure to the initial blanket temperature of 400 °C.

### 3.3 Results and Discussion

Figure 3.1 shows the resulting equilibrium blanket temperatures for the various breeders under consideration, plotted against the reacting percentage of available water. A number of interesting results are noted.

First, as expected, the pure lithium breeding blanket reached the highest temperature upon reaction with water. The dotted line signifies that with a high percentage of available water reacting, some of the unreacted lithium will begin to vaporize at a temperature also close to the melting point of steel. This indicates a potential for further problems if a steel blanket liner is used.

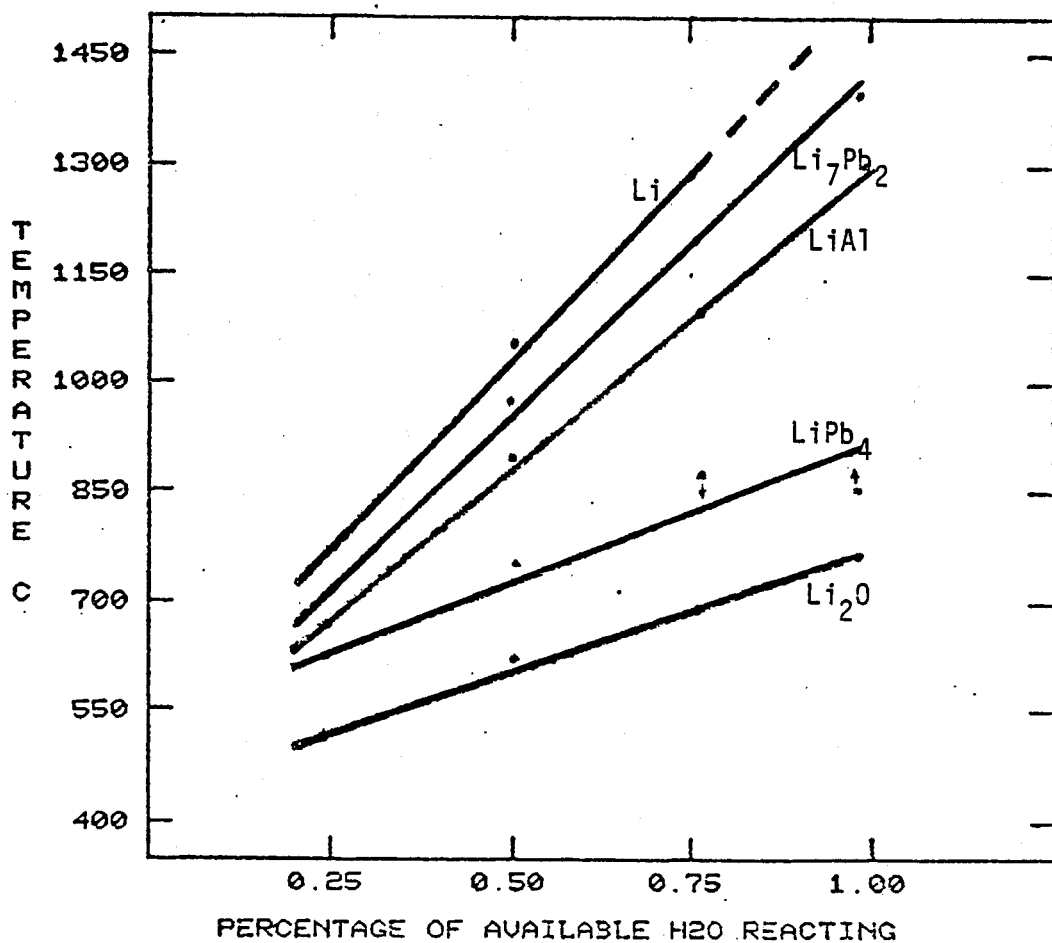


Figure 3.1 Equilibrium Final Temperature Profiles for Various Breeders in the Static Calculation.

$\text{Li}_7\text{Pb}_2$  and  $\text{LiAl}$  are very much alike. Though lower equilibrium temperatures are exhibited than those of the pure lithium breeder, the difference is not very large to be significant. At low percentages of reacting available water, there is no difference.

$\text{Li}_2\text{O}$  and  $\text{LiPb}_4$ , on the other hand, appear to be significantly "cooler" than the pure lithium case. In the case of  $\text{Li}_2\text{O}$ , the key difference is a very low heat of reaction with water.  $\text{LiPb}_4$ , with a relatively high density, is the only case in which there exists more available water than breeder. Thus, a limited heat of reaction and large residue of lead leads to reduced equilibrium temperatures.

## CHAPTER 4. DYNAMIC CALCULATION USING LITFIRE

### 4.1 Introduction

Though valuable as a reference, the calculations of Chapter 3 have little to do with a plausible internal blanket breeder-coolant interaction. It is incorrect to assume that these materials will react instantly at a constant temperature; it is imprudent to declare that the flow of cooling water will cease and that all heat will be retained within the blanket perimeter. Clearly, a dynamic formulation is needed.

To this end, the LITFIRE computer code is modified to estimate the thermal response of the NUWMAK blanket to possible accidents. In this modification, called the internal blanket accident option, the breeder and water react in a zone located in the middle of the breeder mass. The leakage of water into this "reaction zone" is determined by the number of broken coolant tubes, set small enough to justify the assumption that this is the limiting effect on the reaction rate. The heat of reaction is transferred to the breeder mass by conduction and free convection, to the blanket liner and shield by further conduction, and out of the blanket via forced convective cooling by unbroken coolant tubes. Figure 4.1 shows the heat flow diagram for this system.

It is hoped this model presents a truer picture of what will happen within the blanket in the event of a cooling system leak. Again, due to uncertainties concerning data and some assumptions, this study can only provide a measure of relative safety, compared with the trials utilizing liquid lithium.

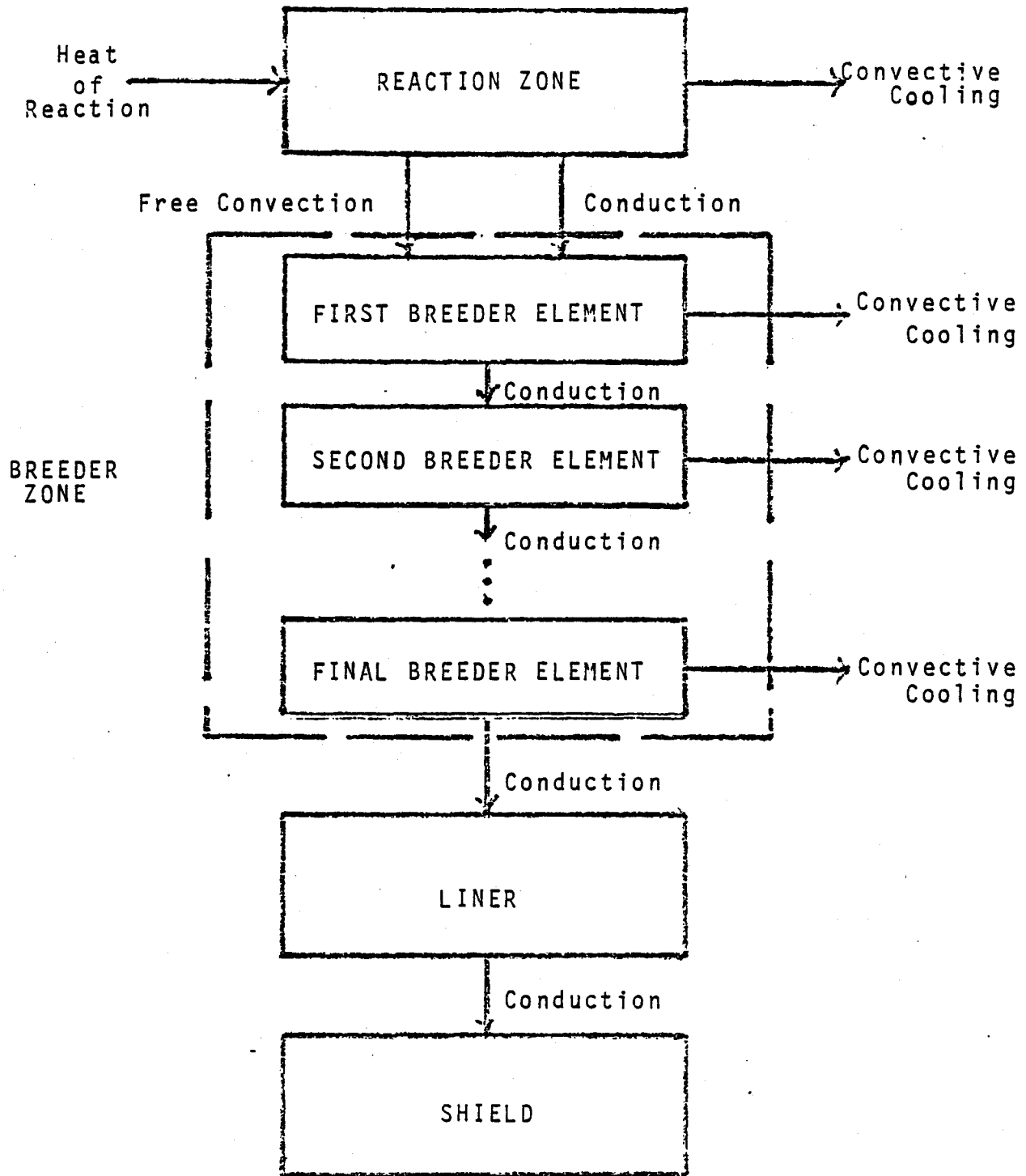


Figure 4.1 Internal Blanket Accident Option Heat Flow Diagram.

#### 4.2 LITFIRE Description

LITFIRE is a computer code developed at MIT [11] to predict the consequences of a hypothetical lithium spill in a fusion reactor containment. It was first written in 1977 as a modification of the Argonne National Laboratory code SPOOLFIRE, used to model the consequences of sodium fires. LITFIRE was later modified and improved in 1980 [3], utilizing the experimental results of small-scale lithium spill tests performed at the Hanford Engineering Development Laboratory.

In this code, the flow of heat is traced from the lithium reaction zone source to reactor containment components, and eventually out to the ambient. This system is simulated by a nodal network in which each node has a heat capacity and temperature equal to that of its physical counterpart. Heat flows between nodes are calculated using standard heat transfer correlations.

To provide the reactor containment thermal and pressure response, LITFIRE solves a set of coupled heat and mass transfer equations. This is done by using the method of finite differences for the spatial dimensions, and either Simpson's rule or a Runge-Kutta method in the time domain [3]. Properties are computed at each time step from the integral equation

$$Y(t) = Y(t_0) + \int_{t_0}^t dt' dY/dt',$$

where the rates of change  $dY/dt$  are given for each node by finite difference solution of the heat transfer relations.



### 4.3 Internal Blanket Accident Option

#### 4.3.1 Assumptions and Structural Model

The internal blanket accident option models an accidental interaction of coolant water and lithium-based breeder in the center of an outside blanket module. This interaction is caused by a breach of several neighboring coolant tubes, while the reactor as a whole undergoes normal operation.

It is assumed that this event is undetected, thus assuring continuance of the plasma burn and coolant recirculation. It is felt that the three monitored parameters relevant to an accident of this type, namely bulk breeding material temperature, coolant temperature, and coolant flow rate, will not change appreciably until later stages of the accident.

The reaction rate is immediate and limited by the leakage of water into the breeding material. The leakage rate, dictated by the number of broken coolant tubes, is set very low, 0.6 kg/sec (three broken tubes), to make this assumption reasonable. Although there is a suspicion that the water reaction rate of the lithium-lead alloys is slow at low temperatures, no data exists. It is also assumed that the reaction zone pressure at high temperatures does not significantly retard the leakage rate of water into the zone.

The reaction zone is very difficult to characterize. However, certain assumptions can be made. First, the zone can be considered spherical, as boiling water at 8.6 MPa will disperse equally in all directions upon tube rupture. The reaction zone must be large enough to accommodate the influx of breeder and coolant, thus the zone radius

should be large compared to the coolant tube pitch length. However, to accommodate the assumption that the water reaction is instantaneous, the reaction zone volume should be small, compared to that of the blanket module.

The initial radius of the reaction zone for three ruptured coolant tubes is set at one foot. This is over six times the characteristic distance separating the three coolant tubes in question. The volume of this zone is less than 2% of the total blanket volume. This seems reasonable for the small leakage rate. Further research in this area would aid the accuracy of the model.

The reaction products (LiOH and alloy element, if any) remain in the reaction zone, thus increasing the radius of this zone with time. The heat capacity of this expanded zone is calculated summing the products of the individual heat capacity of each component multiplied by the weight percent.

The nodal structure of this system is shown in Figure 4.2. It can be seen that the reaction zone and breeder mass are broken into a number of sections. This is to more accurately account for heat transfer by conduction. The number of sections in each zone is selected so as to keep the element widths to approximately 6 inches. These elements increase and decrease in width with time in the reaction zone and breeder zone, respectively, as the reaction zone expands.

The blanket elements are spherical, like the reaction zone, to facilitate computation. The outer element is therefore irregularly shaped to account for the NUWMAK geometry. This is not expected to create any difficulty, as it is doubtful that much heat will be

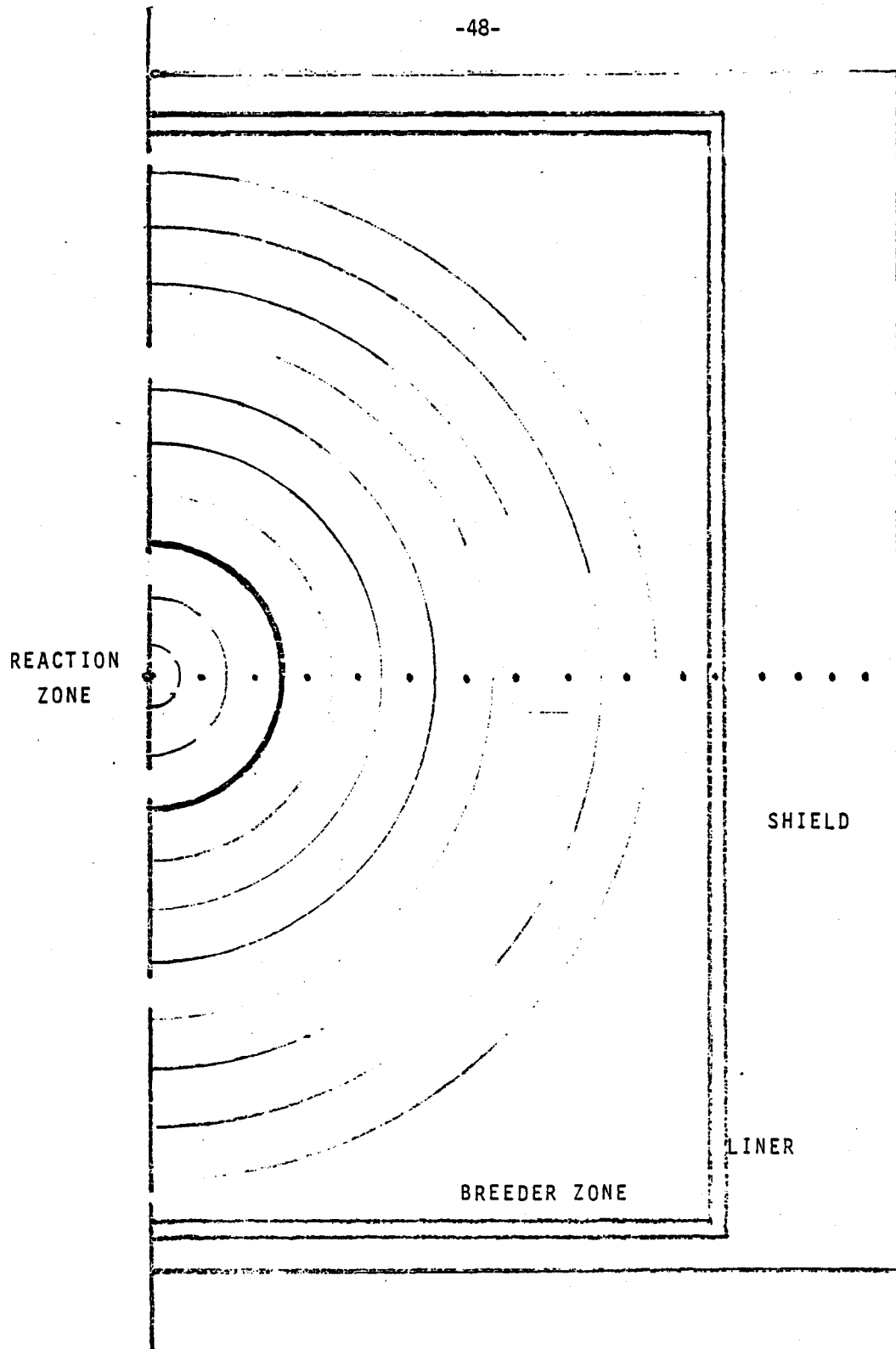


Figure 4.2 Internal Blanket Accident Option Node Structure.

transferred to this region. For completeness, the steel liner and B<sub>4</sub>C shield are also monitored in the code. The conduction of heat is assumed to stop at the far edge of the shield.

The heat of reaction is distributed evenly throughout the reaction zone, heating the reactants and reaction products. Heat is removed by conduction and free convection to the breeder zone, and via forced convection by unbroken coolant tubes as shown in Fig. 4.1. The surface area of cooling tubes in each element is calculated as a volume percentage of the total.

Finally, it should be noted that the densities and thermal conductivities of the lithium-lead alloys and other alternate breeders are held constant with temperature in this analysis. As discussed in the appendix, this data has only been determined at one temperature. Rather than increase uncertainties with various correlations, the values are unaltered.

#### 4.3.2 Heat Transfer Mechanisms

##### A. Heat of Reaction

All of the alternate breeders considered in this study react to some extent with water. Table 4.1 shows the reactions of interest. Other reactions also take place, such as the production of Li<sub>2</sub>O<sub>2</sub>, but are discarded as they play a very minor role. For example, the peroxide is unstable above 250 °C [11] and is not produced above that temperature.

Reaction occurs at the reaction zone temperature T<sub>CZ</sub>. The heat of reaction can be calculated using

$$\Delta H_R = H_{25}^{\circ} + \sum \Delta H_{\text{prod}} - \sum \Delta H_{\text{react}}, \quad \text{Btu/lb breeder} \quad (4.1)$$

TABLE 4.1

Breeder-Coolant Reactions of Interest

	$\Delta H_{\text{hyd}}$ (kJ/g-atom of Li)
$\text{Li} + \text{H}_2\text{O} \rightarrow \text{LiOH} + 1/2 \text{H}_2$	205
$1/7 \text{Li}_7\text{Pb}_2 + \text{H}_2\text{O} \rightarrow \text{LiOH} + 1/2 \text{H}_2 + 2/7 \text{Pb}$	200
$\text{LiPb}_4 + \text{H}_2\text{O} \rightarrow \text{LiOH} + 1/2 \text{H}_2 + 4\text{Pb}$	170
$\text{LiAl} + \text{H}_2\text{O} \rightarrow \text{LiOH} + 1/2 \text{H}_2 + \text{Al}$	200
$\text{Li}_2\text{O} + \text{H}_2\text{O} \rightarrow 2\text{LiOH}$	64

where  $H_{25}^{\circ}$  is the standard heat of hydrolysis at 25 °C and  $\Delta H_{\text{prod}}$  and  $\Delta H_{\text{react}}$  are the enthalpy changes of the reaction products and reactants, respectively, as they are heated from 25 °C to  $T_{\text{CZ}}$ .

Since the reaction is immediate, limited by the leakage of water into the reaction zone, the reaction rate is the leakage rate. This can be written as

$$R_w = \dot{m} N_T \quad \text{lb H}_2\text{O/sec} \quad (4.2)$$

where  $\dot{m}$  is the mass flow rate of water through one tube and  $N_T$  is the number of ruptured tubes. Thus, the total heat generation rate inside the reaction zone can be given by

$$Q = a_0 \Delta H_R \dot{m} N_T \quad \text{BTU/sec} \quad (4.3)$$

where  $a_0$  is the stoichiometric combination constant for the breeder and water in the given reaction.

#### B. Sensible Heat Addition to Reactants in the Reaction Zone

A portion of the heat of reaction is used to heat the inflowing coolant water and breeder to the reaction zone temperature. This can be written as

$$Q_s = N_T \dot{m}_w c_w (T_{\text{CZ}} - T_c) + \dot{m}_b c_b (T_{\text{CZ}} - T_L) \quad \text{BTU/sec} \quad (4.4)$$

where  $\dot{m}_w$  is the mass flow rate of water in a coolant tube  
 $c_w$  is the mean specific heat of the coolant

$\dot{m}_b$  is the mass influx of breeder to the reaction zone

$c_b$  is the mean specific heat of the breeder

$T_c$  is the coolant temperature

$T_L$  is the bulk breeder temperature.

In this case, the influx of breeder into the reaction zone is considered equal to the leakage rate of the coolant into the zone, as reaction is immediate. This mass transfer is further discussed in the free convection section.

### C. Forced Convective Cooling

Forced convection, due to the continued coolant recirculation through undamaged tubes, is an important heat transfer mechanism. Because only a small number of the 475 coolant tubes in an outside blanket module are damaged, cooling will take place in both the breeding and reaction zones. The cooling tube surface area in each element can be determined as a volume percentage of the blanket as a whole. For example, the initial reaction zone, approximately 2% of the blanket by volume, comes into contact with roughly 2% of the total cooling tube surface area. This total area can be determined using the information in Table 2.7.

This total heat flow can be computed for each element using

$$Q_c = \left[ \frac{\delta}{k_{Ti} A_{SO}} + \frac{1}{h A_{SI}} \right]^{-1} (T_i - T_c) \quad \text{BTU/sec} \quad (4.5)$$

where  $\delta$  is the coolant tube thickness

$k_{Ti}$  is the thermal conductivity of the titanium alloy

$A_{SO}$  is the outer coolant tube surface area

$A_{SI}$  is the inner coolant tube surface area

$h$  is the boiling water heat transfer coefficient

$T_i$  is the bulk temperature of the element in question.

#### D. Conduction

Conduction plays a major role in the transfer of heat from the reaction zone to the breeder mass. The heat conduction term between two elements can be expressed as

$$Q_{\text{cond}_{ij}} = A_i \left[ \frac{k_i k_j}{k_i + k_j} \right] (T_i - T_j) / d_{ij} \quad \text{BTU/sec} \quad (4.6)$$

where  $A_i$  is the inner element surface area

$k_i$  is the inner element thermal conductivity

$k_j$  is the outer element thermal conductivity

$T_i$  is the inner element bulk temperature

$T_j$  is the outer element bulk temperature

$d_{ij}$  is the separation distance between the elements.

The surface area assigned to each element is at its outer perimeter. In the above expression, it is assumed that the inner element is at a higher temperature, as is the case at all times in the LITFIRE option.

#### E. Free Convection

A preliminary order of magnitude analysis indicates that the free convective enhancement to conduction is  $Pr Gr^{1/2}$ , where  $Pr$  and  $Gr$  are the Prandl and Grashof numbers. For a 400 °C temperature



difference between the reaction and breeder zones in the lithium case, this enhancement is better than a factor of ten. Thus, free convection is an important mode of heat transfer in the model.

As mentioned before, there will be mass transfer in the breeding zone due to the influx of this material into the reaction zone. It is this movement that allows convective cooling of the reaction zone by the first breeder zone element.

Given the spherical shape of the reaction zone, the semi-empirical relation

$$\overline{Nu} = 2.0 + 0.60 Gr^{1/4} Pr^{1/3} \quad (4.7)$$

is useful to find the average heat transfer coefficient for  $Gr^{1/2} \cdot Pr^{1/3} < 200$ .  $\overline{Nu}$  is the average Nusselt number and is related to the average heat transfer coefficient  $\overline{h}_m$  by

$$\overline{Nu} = \overline{h}_m L/k \quad (4.8)$$

where  $L$ , the characteristic distance, is in this case the reaction zone diameter.

Thus, the heat flow due to free convection can be described by

$$Q'_c = \frac{A_{cz} k_b}{D} (2.0 + 0.60 Gr^{1/4} Pr^{1/3})(T_{cz} - T_L) \frac{BTU}{sec} \quad (4.9)$$

where  $A_{cz}$  is the reaction zone surface area and  $k_b$  is the bulk breeder thermal conductivity.  $Gr = \frac{D^3 \rho^2 g \beta \Delta T}{\mu^2}$  and  $Pr = \frac{c_p \mu}{k}$  are applicable to

the fluid breeders.

#### F. Radiation

Using an order of magnitude analysis, the radiative heat flow is related to the conductive heat flow by

$$Q_{\text{rad}} = \frac{\sigma T^3 L}{k} Q_{\text{cond}} \quad (4.10)$$

where  $\sigma$  is the Stefan-Boltzmann constant. At 1500 °F, this radiative heat flow is a factor of ten less than that of conduction in a lithium breeder. Therefore, radiation is neglected in the model.

#### 4.3.3 The Numerical Scheme

The temperature of a thermal element may be found from the solution to

$$mc \frac{dT}{dt} = q_1 + q_2 + q_3 + \dots, \quad T = T_0 \text{ at } t = t_0, \quad (4.11)$$

where  $mc$  is the element's heat capacity and  $q_1, q_2, q_3 \dots$  are heat flows into the element, shown in Fig. 4.1. This may also be expressed as

$$T = \int_{t_0}^t \frac{1}{mc} (q_1 + q_2 + q_3 + \dots) dt + T_0. \quad (4.12)$$

In LITFIRE, this is expressed as

$$T = \text{INTGRL} (T_0, dt/dt). \quad (4.13)$$

A set of sub-routines is used to perform the integrations using either Simpson's Rule or a Runge-Kutta method.

For example, heat flows into the reaction zone are the heat of reaction, sensible heat addition to the reactants, conduction, free convection and forced convective cooling. Therefore, the temperature of the reaction zone at time  $t$  can be determined in LITFIRE by using Eq. (4.13) and

$$\frac{dT}{dt} = \frac{1}{mc} [Q - Q_s - Q_{CR} - Q_{\text{cond}_{RL1}} - Q'_C] \quad (4.14)$$

where the subscript R denotes the reaction zone and L1 denotes the first breeder element.  $Q$ ,  $Q_s$ ,  $Q_{CR}$ ,  $Q_{\text{cond}_{RL1}}$ , and  $Q'_C$  can be determined using Equations (4.3), (4.4), (4.5), (4.6), and (4.9), respectively. Similar equations can be written for each thermal element in the model.

#### 4.4. Results and Discussion

Figure 4.3 shows the thermal response of the reaction zone (TCZ), first breeder element (TLI1) and middle breeder element (TLI4) over the first 1000 seconds for a lithium breeder accident, as described earlier in this chapter. Similar graphs are plotted in Figures 4.4 through 4.7 for  $\text{Li}_7\text{Pb}_2$ ,  $\text{LiPb}_4$ ,  $\text{LiAl}$  and  $\text{Li}_2\text{O}$  breeders, respectively. A number of interesting points are noted.

First, the general shapes of the curves in each case are similar, although different maximum temperatures are attained. A change of time step shows no appreciable difference. The reaction zone rises rapidly, reaching a maximum value within the first two minutes of the coolant tube breaks. Thereafter, the temperature decreases monotonically,

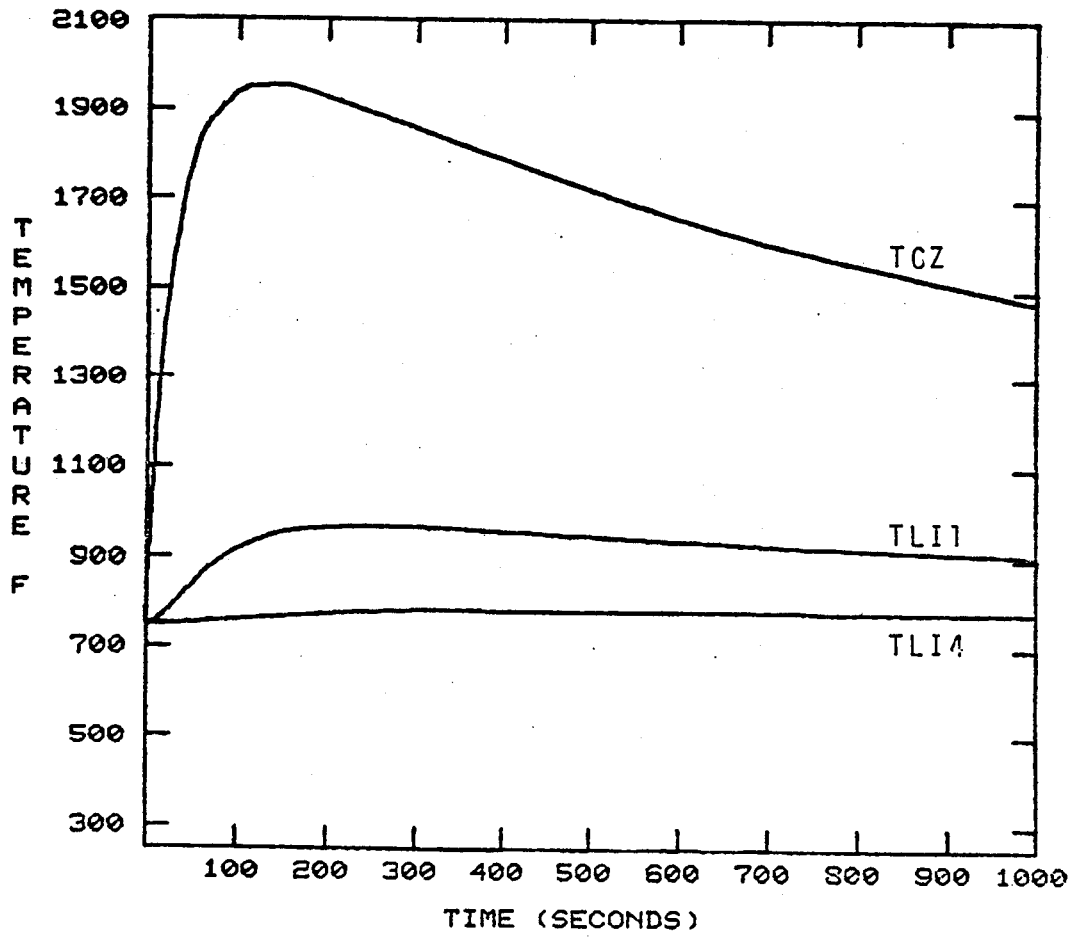


Figure 4.3 Lithium Breeder Thermal Response to Water Interaction.

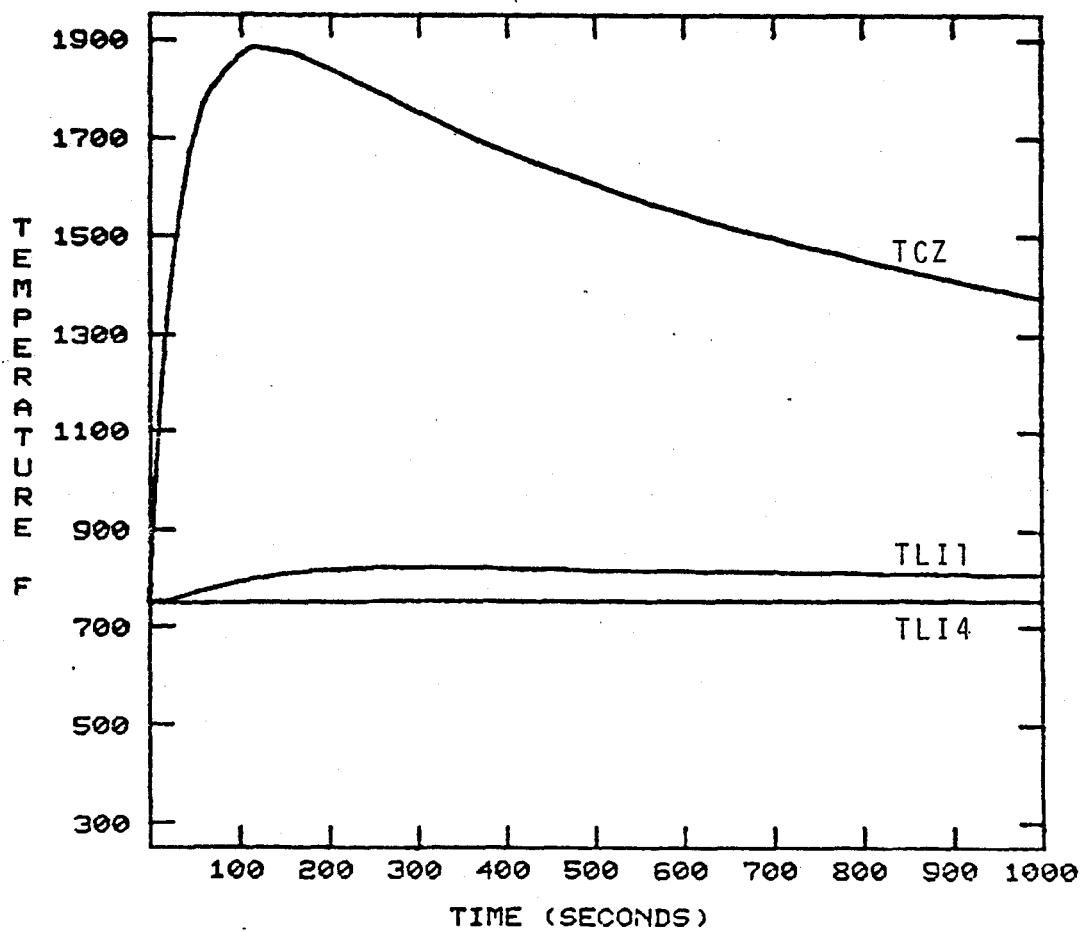


Figure 4.4  $\text{Li}_7\text{Pb}_2$  Breeder Thermal Response to Water Interaction.

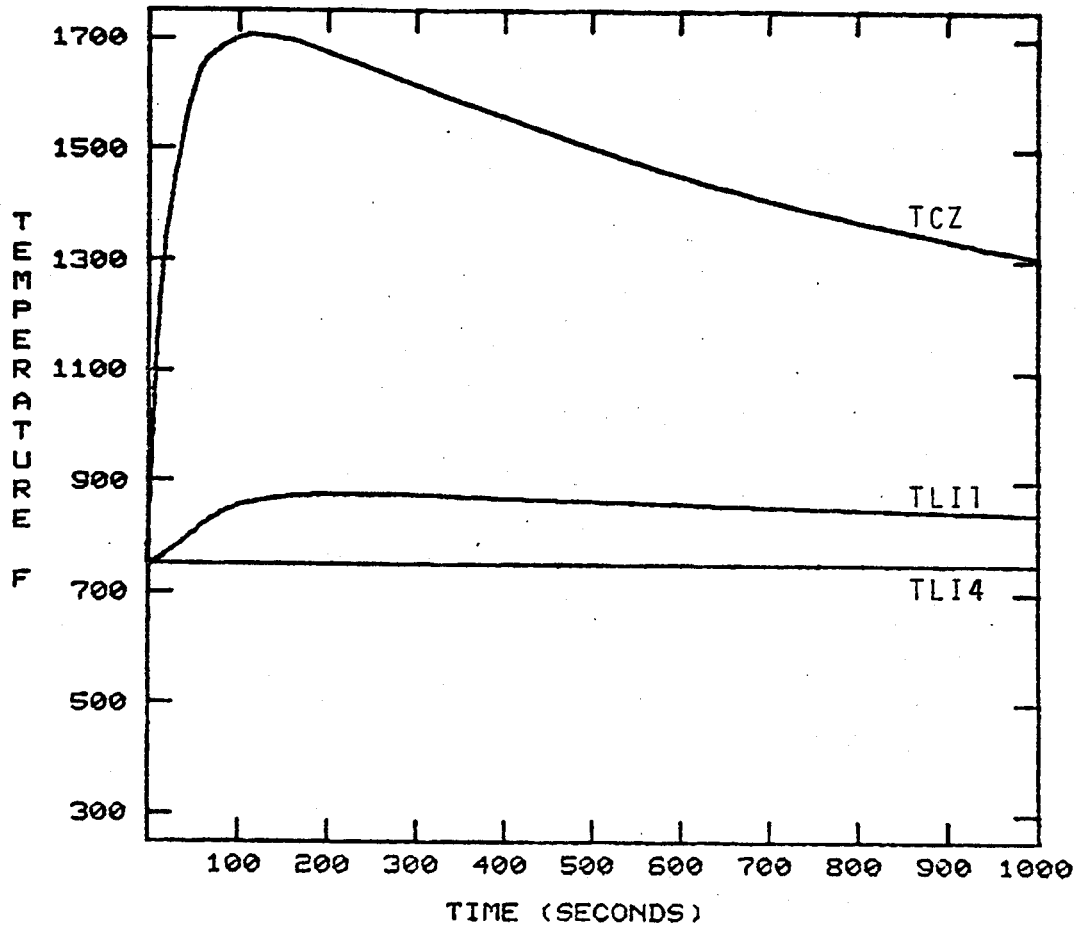


Figure 4.5 LiPb<sub>4</sub> Breeder Thermal Response to Water Interaction.

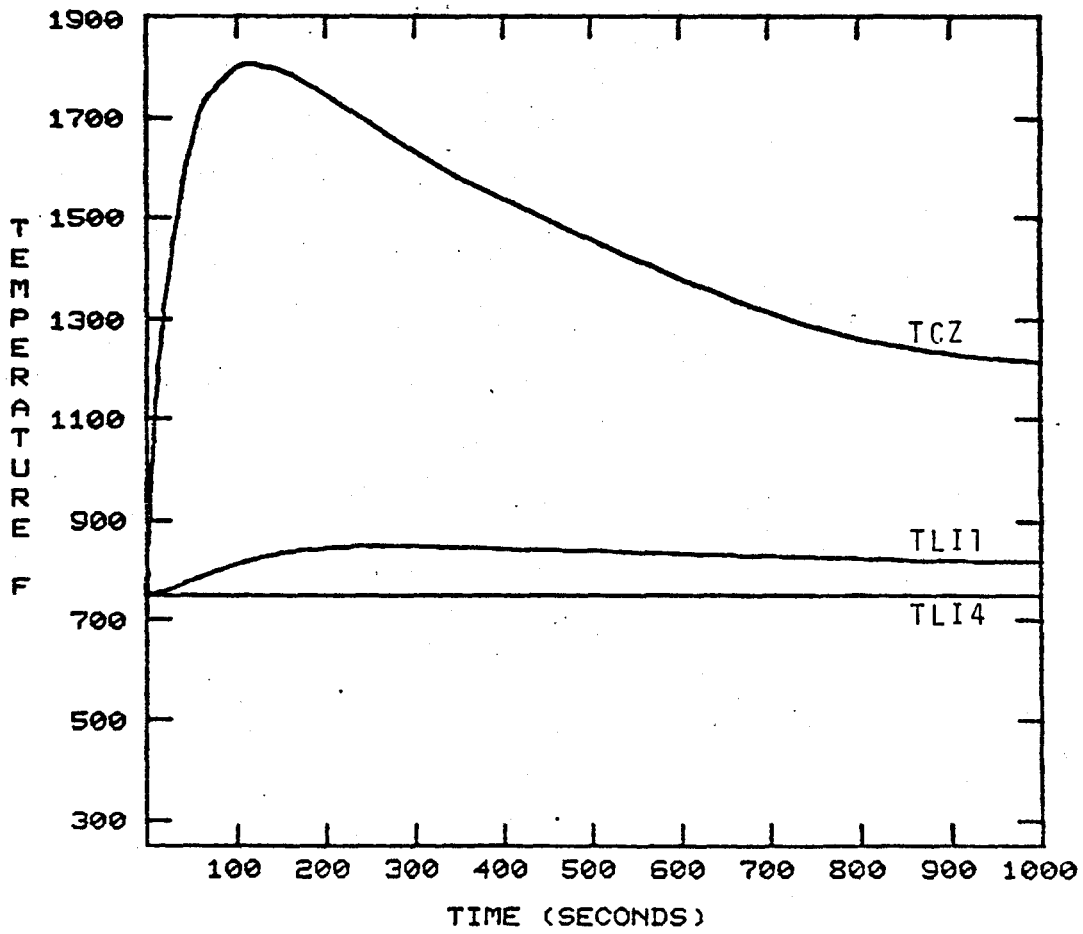


Figure 4.6 LiAl Breeder Thermal Response to Water Interaction.

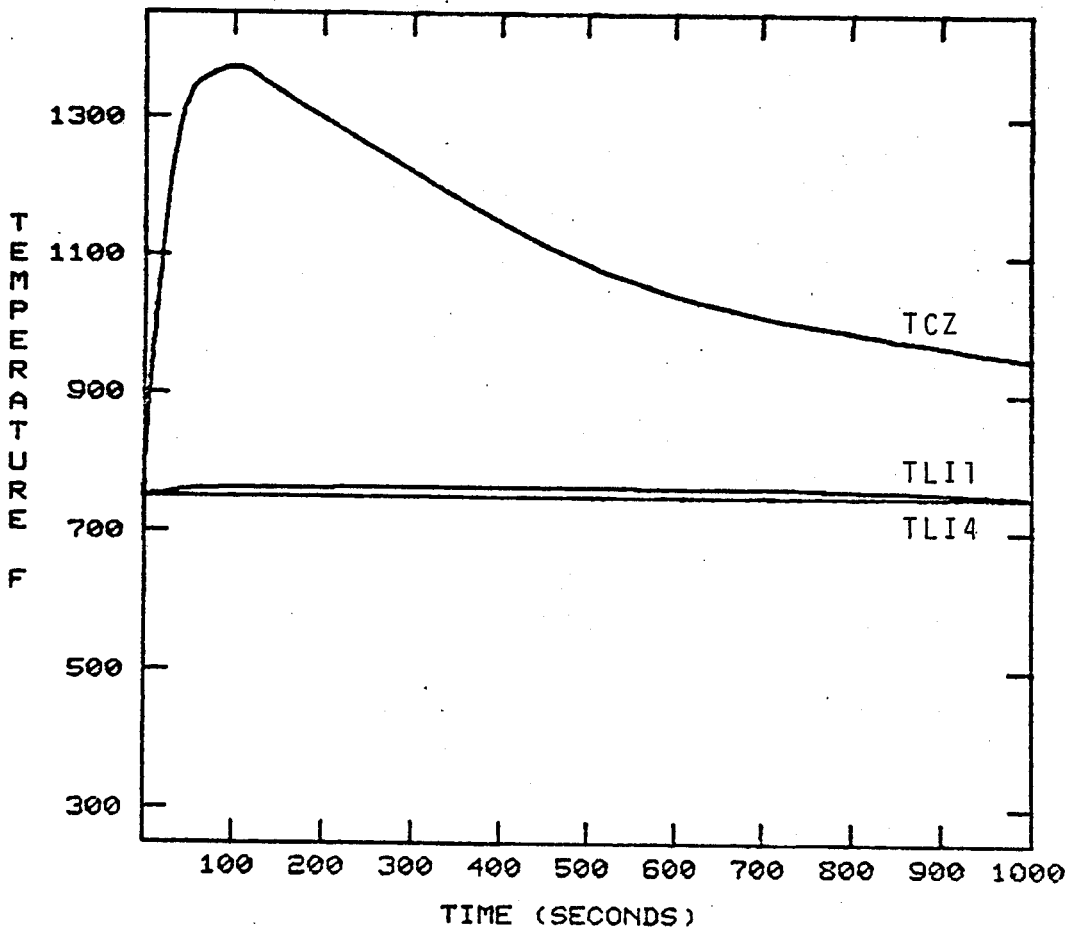


Figure 4.7  $\text{Li}_2\text{O}$  Breeder Thermal Response to Water Interaction.



more gradually as time progresses. The first blanket element exhibits similar behavior, but at lower temperatures and lagging over a minute behind. The middle blanket element is relatively unchanged, slowly increasing 50 °F in the lithium case and nearly constant in the alternate breeders.

This behavior may be due to different characteristic times for the various heat transfer processes. The heat of reaction in the reaction zone is instantaneous and relatively large compared to the conductive and convective flows, thus a rapid initial rise. Eventually, as the temperature difference between the reaction zone and first breeder element increases, so do the conductive and convective flows and the temperature profile flattens and decreases. Thereafter, as this temperature difference decreases, the reaction zone temperature decreases more gradually. This continues until the breeder (or water, in the  $\text{LiPb}_4$  case) is depleted, eliminating the heat of reaction. Thereafter, all zones are eventually recooled to 752 °F. The first 1000 seconds are shown as the entire process takes upwards to 11 hours ( $4 \times 10^4$  seconds).

The relatively small volume of the reaction zone (less than 2% of the blanket module volume) may account for both the high temperatures attained in the reaction zone and the large temperature difference between this zone and the first breeder element (approximately 1000 °F in the lithium run). A small volume implies a small mass and surface area. The small mass is very sensitive to the heat of reaction and the small surface area impedes conductive and convective flows out. As the reaction zone expands, this effect is diminished.

The blanket liner, shield and other breeder elements were also monitored. All zones outside of the fourth breeder element showed no significant change. Thus, the accident appears to be effectively localized. The second and third breeder elements showed similar behavior as the first, with progressively shorter time lags.

Figure 4.8 presents a comparison of the reaction zone temperature profiles for the various breeders. As expected, the liquid lithium breeder produces the highest temperatures. Also expected, using the results of Chapter 3 as reference, is that the  $\text{Li}_2\text{O}$  breeder temperatures are significantly less. This breeder has a definite safety advantage compared to pure lithium.

The same can not be said, however, of the lithium-lead breeders and  $\text{LiAl}$ . Though less, the resulting temperatures are well within the range of the lithium case, as close as  $70^\circ\text{F}$  ( $\text{Li}_7\text{Pb}_2$ ) and not further apart than  $250^\circ\text{F}$  ( $\text{LiPb}_4$ ). These differences are insignificant at a base temperature of  $1950^\circ\text{F}$ .

This result was surprising in the case of  $\text{LiPb}_4$ . Equation (4.14) indicates that the temperature rate of change in the reaction zone is inversely proportional to the reaction zone mass. Since the reaction zone volume is initially fixed and there is a factor of 20 increase in the density of  $\text{LiPb}_4$  over that of  $\text{Li}$  (at  $400^\circ\text{C}$ , the density of  $\text{Li}$  is  $0.51\text{ g/cm}^3$ ; the density of  $\text{LiPb}_4$  is  $9.9\text{ g/cm}^3$ ), it was felt that the temperature rise would be proportionally decreased.

However, a closer look at Eq. (4.14) indicates that the temperature rate of change is also inversely proportional to the reaction zone specific heat. In this case, the specific heat of  $\text{LiPb}_4$ , approximately

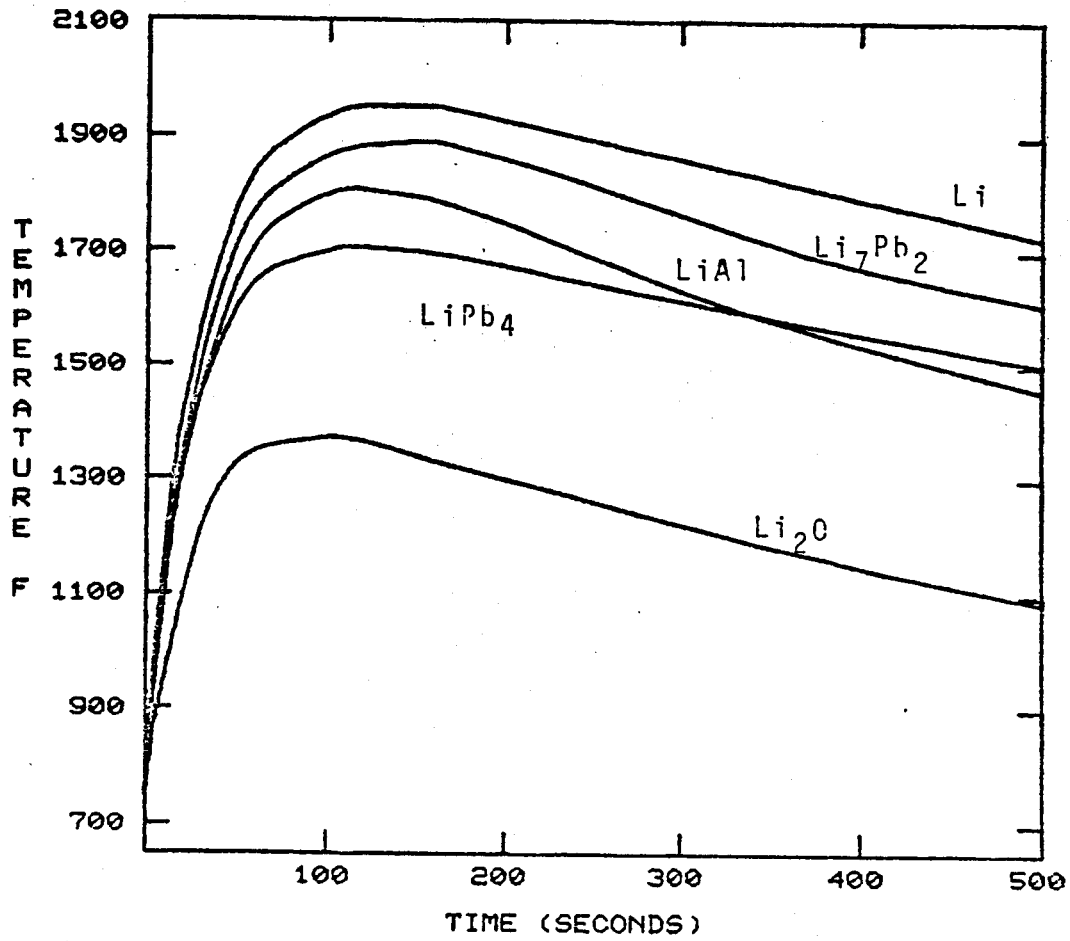


Figure 4.8 Comparison of Reactor Zone Temperature Profiles of the Various Breeders.

that of Pb, is nearly a factor of 20 less than that of pure lithium (at 400 °C, the specific heat of lithium is 1.01 cal/g - °F; that of  $\text{LiPb}_4$  is 0.041 cal/g - °F). Thus, the terms in the denominator of Eq. (4.14) effectively cancel each other out and the slightly different reaction zone temperature profiles of Li and  $\text{LiPb}_4$  are simply a reflection of the slightly different heats of reaction of the two breeders with water.

A comparison of the thermal responses of the first breeder elements for the various breeders, shown in Fig. 4.9, is also interesting. Again, the lithium case produces the highest temperatures and the  $\text{Li}_2\text{O}$  case produces the lowest. The lithium-lead alloy and LiAl results are again similar. Here the  $\text{Li}_7\text{Pb}_2$  element is cooler overall due to a very low thermal conductivity, experienced in the lithium-lead system at a 20% lithium atom percentage [13]. However, in this comparison, the differences between these alloys and the lithium case are more pronounced. This indicates that the use of liquid lithium will produce more widespread accidental consequences.

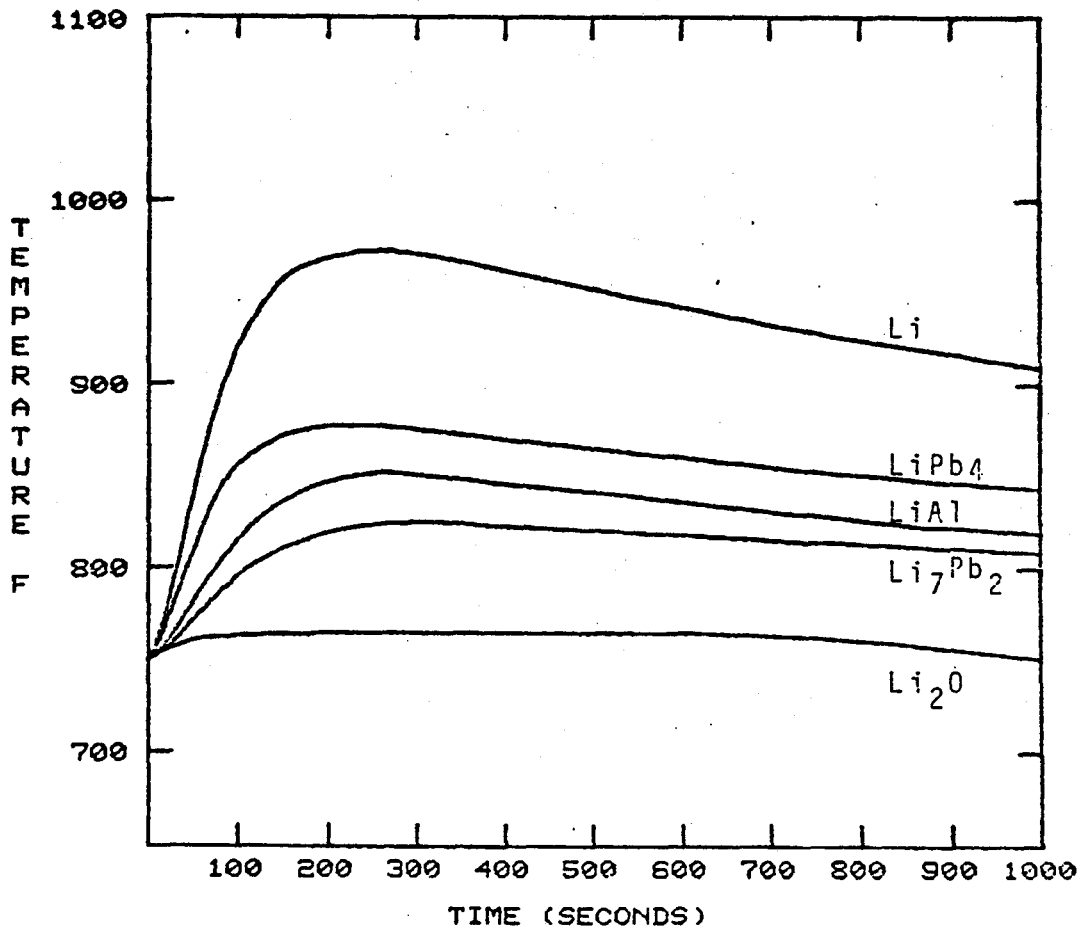


Figure 4.9 Comparison of First Breeder Element Temperature Profiles of the Various Breeders.

## CHAPTER 5. CONCLUSIONS AND RECOMMENDATIONS

Results indicate that the lithium-lead alloys may not be significantly safer than pure lithium as a fusion reactor breeding material, utilizing the NUWMAK geometry. In both calculations, short term temperatures resulting from interaction of  $\text{Li}_7\text{Pb}_2$  and  $\text{LiPb}_4$  with water, though lower, are within a few hundred degrees of those associated with the use of liquid lithium.

However, a proper conclusion to this study is that a conclusion cannot yet be made. The calculations of Chapters 3 and 4 provide an overview of the safety question, raising some interesting observations and determining areas that need to be explored in more detail.

First, the lithium-lead alloys and  $\text{LiAl}$  can pose safety problems approximate to those of liquid lithium, as noted above. This can be quite serious, as shown in Chapter 3, with temperatures reaching to the melting point of steel in a water-cooled blanket. For this reason alone, further study of these alternate breeders is required.

Results of Chapter 4 indicate that such an interaction could go undetected, as a continuance in coolant recirculation may keep the consequences localized. Measurable quantities, like bulk breeder temperature and coolant temperature and flow rate are practically unperturbed. Thus, further design work might include features to mitigate this problem.

Uncertainties in characterizing the reaction zone in the dynamic model render the resulting temperature profiles less meaningful. Further work in this area, perhaps experimental, would make the model more accurate.

Finally, better physical properties data on the alternate breeders is required. In particular, an understanding of the water reaction rates is central to the study of these materials. If it can be proved, as surmized, that these rates are significantly lower than those of liquid lithium, a significant reduction in safety hazards may be assured.

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APPENDIX A  
Physical Property Data



Table A.1 summarizes the important physical property data of the various alternate breeders analyzed in this report. Except as indicated, all of these values are gathered from the previously identified references. It is important to realize that, aside from the lithium and melting point data, all numbers are estimates at best.

For reasons detailed earlier, only the physical properties of the lithium breeder are allowed to vary with temperature in calculations of Chapters 3 and 4. The correlations used are:

$$\begin{aligned}\rho &= 0.5368 - 1.0208 \times 10^{-4}T \text{ (g/cm}^3\text{)} \\ k &= 10.48 + 4.98 \times 10^{-3}(T - 180.6) - 0.58 \times 10^{-6}(T - 180.6)^2 \\ &\quad \text{(cal/sec-m-}^\circ\text{C)} \\ c_p &= 1.0037 - 0.01063x + 0.00564x^2 - 0.001279x^3 \text{ (cal/g }^\circ\text{C)} \\ &\quad \text{where } x = .004938T - 6.20741\end{aligned}$$

Here,  $\rho$  = density of lithium  
 $k$  = thermal conductivity of lithium  
 $c_p$  = specific heat of lithium  
 $T$  = lithium temperature in  $^\circ\text{C}$

The latent heats of melting for the alloy breeders are determined using the correlation

$$H_{\text{melt}}/T_{\text{melt}} \sim 2.2$$

This is an average value for metallic alloys [14].

The thermal conductivity of  $\text{LiPb}_4$  is estimated with the correlation

$$k_m = k_1 w_1 + k_2 w_2 - 0.72(k_2 - k_1)(w_1 w_2)$$

This is appropriate for a binary liquid mixture. Here, the weight fraction  $w_2$  refers to the component having the larger value of  $k$  [14].

The specific heat data of the alloy breeders is determined using the relation

$$c_{p\text{alloy}} = X_{\text{Li}} c_{p\text{Li}} + X_{\text{A}} c_{p\text{A}}$$

where

$X_{\text{Li}}$  = weight fraction of lithium

$X_{\text{A}}$  = weight fraction of the alloy element

$c_{p\text{A}}$  = specific heat of the alloy element

$c_{p\text{Li}}$  = specific heat of lithium

The specific heat values for the alloy elements, lead and aluminum, can be found in the literature.

TABLE A.1

Summary of Physical Properties of Candidate Breeding Materials at Standard Conditions

<u>Properties</u>	<u>Lithium</u>	<u>Li<sub>7</sub>Pb<sub>2</sub></u>	<u>LiPb<sub>4</sub></u>	<u>LiAl</u>	<u>Li<sub>2</sub>O</u>
Melting Point, °K	453	999	508	973	1970
$\Delta H_{\text{melt}}$ , cal/g mole	722.4	2200 <sup>a</sup>	1120 <sup>a</sup>	2140 <sup>a</sup>	—
Density, g/cm <sup>3</sup>	0.51	4.59	9.9	1.76	2.01
Li atom density, g/cm <sup>3</sup>	0.51	0.49	0.08	0.37	0.93
Thermal conductivity w/m-k	50	~20	~35 <sup>a</sup>	30	1.73
Specific Heat cal/g °K	1.01	0.14 <sup>b</sup>	0.041 <sup>b</sup>	0.44 <sup>b</sup>	0.35
Heat of Reaction with Water kJ g-atom Li	245	200	170 <sup>c</sup>	200	64
Atomic weight	7	463	835	34	30

a. correlation

b. interpolated value

c. estimated



APPENDIX B  
Complete Listing of LITFIRE





C LITFIRE COMPUTER CODE IS A MODIFICATION OF THE CODE SPOOL-FIRE DELIT00010  
 C AT ARGONNE NATIONAL LABORATORY. LITFIRE DESCRIBES THE TEMPERATURE LIT00020  
 C PRESSURE HISTORY OF A FUSION REACTOR CONTAINMENT TO LITHIUM FIRE LIT00030  
 C AND WAS DEVELOPED IN THE NUCLEAR ENGINEERING DEPARTMENT AT MIT IN LIT00040  
 C LIT00050  
 C THIS VERSION OF LITFIRE HAS A MANDATORY ONE NODE IN THE LITHIUM LIT00060  
 C POOL, WITH A SUSPENDED (INSULATED) PAN OPTION LIT00070  
 C THE CONTAINMENT IS SINGLE CELL LIT00080  
 C DEFINITION OF VARIABLES AND UNITS LIT00090  
 C LIT00100  
 C THIS IS A RELATIVELY COMPLETE LISTING OF THE VARIABLES, CONSTANTS, LIT00110  
 C PARAMETERS USED IN THE COMPUTER CODE LITFIRE II, ACCURATE AS OF LIT00120  
 C SEPTEMBER 30, 1980. FURTHER DOCUMENTATION AND SOME DERIVATIONS LIT00130  
 C MAY BE FOUND IN THE LITFIRE PROGRAMMER'S MANUAL LIT00140  
 C LIT00150  
 C AINS OUTSIDE EXPOSED AREA OF INSULATING LAYER ON PAN (FT2) LIT00160  
 C AKLI THERMAL CONDUCTIVITY OF LITHIUM BTU/FT.-SEC. DEG. F LIT00170  
 C INPUT AS BTU/FT. HR. DEG. F LIT00180  
 C AK1, AK2 PROD. OF THERMAL COND. AND PRANDTL NO. BTU/SEC-FT-DEG. LIT00190  
 C AMLI ATOMIC MASS OF BREEDER LIT00200  
 C AMPB ATOMIC MASS OF ALLOY METAL LIT00210  
 C APAN PAN EXTERNAL AREA FOR HEAT TRANSFER LIT00220  
 C ARE SURFACE AREA OF BREEDER ELEMENT LIT00230  
 C ASLI SURFACE AREA OF LITHIUM FT2 LIT00240  
 C ATI INNER SURFACE AREA OF COOLANT TUBES IN ELEMENT LIT00250  
 C ATO OUTER SURFACE AREA OF COOLANT TUBES IN ELEMENT LIT00260  
 C AW EXPOSED WALL AREA FT2 LIT00270  
 C AWA AREA OF THE STEEL CONTAINMENT BELOW THE SPILL PAN FT LIT00280  
 C B USED IN CALC. THERMAL RESIST. OF LINER-GAP-CONC. FT. LIT00290  
 C BB ANALOGOUS TO B, ONLY FOR FLOOR CONCRETE LIT00300  
 C B1 & B2 COEFFICIENT OF GAS EXPANSION 1/DEG. F LIT00310  
 C BLIN TIME AFTER SPILL AT WHICH INERT GAS FLOODING AND LIT00320  
 C EXHAUST BEGINS SEC LIT00330  
 C BLOUT TIME AFTER SPILL AT WHICH FLOODING AND EXHAUST STOPS SECLIT00340  
 C BLOWR INERT GAS INPUT RATE LB/SEC LIT00350  
 C BLOW INERT GAS INPUT RATE FT3/MIN LIT00360  
 C BREDTH LENGTH AROUND THE SIDE OF THE SPILL PAN IN FEET LIT00370  
 C \*\*\* "C" IS THE INITIAL USED FOR INDICATING A THERMAL DIFFUSIVITY. LIT00380  
 C CONDUCTIVITY BETWEEN TWO NODES DIVIDED BY THE HEAT CAPACITY OF ONLIT00390  
 C THOSE NODES LIT00400  
 C C1 CONTAINMENT GAS TO WALL STEEL IN GAS LIT00410  
 C C2 PAN TO CONT GAS IN GAS LIT00420  
 C C3 STEEL LINER TO CONCRETE WALL IN WALL CONCRETE LIT00430  
 C C4(I) CONCRETE NODE I TO NODE I+1 IN WALL CONCRETE LIT00440  
 C C5 CONCRETE WALL TO AMBIENT IN CONCRFTE LIT00450  
 C C6 CONTAINMENT GAS TO WALL STEEL IN STEEL LIT00460  
 C C7 STEEL LINER TO CONCRETE WALL IN STEEL LIT00470  
 C C8 STEEL LINER TO CONCRETE FLOOR IN STEEL LIT00480  
 C C9 STEEL LINER TO CONCRETE FLOOR IN CONCRETE LIT00490  
 C C10(I) CONCRETE FLOOR NODE I TO NODE I+1 IN FLOOR CONCRETE LIT00500  
 C C11 STEEL TO AMBIENT (NO CONCRETE OPTION) IN STEEL LIT00510  
 C C12 PAN TO GAS IN PAN LIT00520  
 C C13 COMBUSTION ZONE TO CONTAINMENT GAS IN GAS LIT00530

C	CCZP	POOL TO COMBUSTION ZONE	IN POOL	LI00540
C	CGCZ	COMBUSTION ZONE TO CONTAINMENT GAS IN COMBUSTION ZONE		LI00550
C	CGLI	POOL TO CONTAINMENT GAS (NO COMBUSTION) IN POOL		LI00560
C	CH	CONTAINMENT HEIGHT	FT	LI00570
C	CIN12	INNER TO OUTER INSULATION	IN INNER INSULATION	LI00580
C	CIN21	INNER TO OUTER INSULATION	IN OUTER INSULATION	LI00590
C	CIN1PN	STEEL PAN TO INNER INSULATION	IN INSULATION	LI00600
C	CLIG	POOL TO CONTAINMENT GAS (NO COMBUSTION) IN GAS		LI00610
C	CLIPAN	POOL TO SPILL PAN IN POOL	(SUSP PAN OPTION)	LI00620
C	CLIST	LITHIUM POOL TO FLOOR STEEL	IN LITHIUM	LI00630
C	CPANLI	POOL TO PAN		LI00640
C	CPCZ	LITHIUM POOL TO COMBUSTION ZONE	IN COMBUSTION ZONE	LI00650
C	CPIN1	STEEL PAN TO INNER INSULATION	IN PAN	LI00660
C	CSBLI	LITHIUM POOL TO FLOOR STEEL	IN STEEL	LI00670
C	CSZ	AMOUNT OF HEAT BEING DEVELOPED IN THE COMB. ZONE	(BTU)	LI00680
C	CMBR	TOTAL COMBUSTION RATE	LB. LI/SEC.-FT2	LI00690
C	CMBRH	TOTAL COMBUSTION RATE	LB. LI/HR.-FT2	LI00700
C	CMBRHI	INITIAL COMBUSTION RATE	LB. LI/HR.-FT2	LI00710
C	CMBRN	COMB. RATE FOR NITROGEN REACTION	LB. LI/SEC.-FT2	LI00720
C	CMBR0	COMB. RATE FOR OXYGEN REACTION	LB. LI/SEC.-FT2	LI00730
C	CMBRW	COMB. RATE FOR WATER VAPOR REACTION	LB. LI/SEC.-FT2	LI00740
C	CPA	INERT GAS SPECIFIC HEAT	BTU/LB.-DEG. F	LI00750
C	CPAB	SPEC. HEAT OF FLOODING GAS	BTU/LB.-DEG. F	LI00760
C	CPCON	HEAT CAPACITY OF FLOOR AND WALL CONCRETE		LI00770
C	CPH2	HEAT CAPACITY OF HYDROGEN GAS		LI00780
C	CPHS	SPECIFIC HEAT OF INSULATION	BTU/LB DEG F	LI00790
C	CPLI	SPECIFIC HEAT OF LI	BTU/LB. -DEG. F	LI00800
C	CPLI1	MEAN HEAT CAPACITY OF BREEDER AS SOLID	BTU/LB MOLL	LI00810
C	CPLIN	SPEC. HEAT OF LITHIUM NITRIDE	BTU/LB.-DEG. F	LI00820
C	CPLIO	SPECIFIC HEAT OF LITHIUM OXIDE	BTU/LB.-DEG. F	LI00830
C	CPLIOH	SPECIFIC HEAT OF LIQH	BTU/LB-MOLE F	LI00840
C	CPMCZ	EFFECTIVE HEAT CAPACITY OF COMB. ZONE	BTU/DEG F	LI00850
C	CPMH2	HEAT CAPACITY OF HYDROGEN IN CONTAINMENT	BTU/DEG. F	LI00860
C	CPMLH	HEAT CAP. OF LITH. HYDROXIDE IN CONT.	BTU/DEG. F	LI00870
C	CPMLIN	HEAT CAP. OF LITH. NITRIDE IN CONT.	BTU/DEG. F	LI00880
C	CPMLIO	HEAT CAP. OF LITHIUM OXIDE IN CONTAINMENT	BTU/DEG. F	LI00890
C	CPMNI	HEAT CAPACITY OF NITROGEN IN CONTAINMENT	BTU/DEG. F	LI00900
C	CPMOX	HEAT CAPACITY OF OXYGEN IN CONTAINMENT	BTU/DEG. F	LI00910
C	CPMWA	HEAT CAP. OF WATER VAP. IN CONTAINMENT	BTU/DEG. F	LI00920
C	CPN2	HEAT CAPACITY OF NITROGEN GAS		LI00930
C	CPPAN	SPECIFIC HEAT OF SPILL PAN	BTU/LB-DEG F	LI00940
C	CPPB	HEAT CAPACITY OF ALLOY METAL IN BREEDER ZONE	BTU/LB-F	LI00950
C	CPPB1	MEAN HEAT CAPACITY OF ALLOY METAL SOLID	BTU/LB MOLE	LI00960
C	CPPL	LIQUID HEAT CAPACITY OF ALLOY METAL	BTU/LB R	LI00970
C	CPPZ	HEAT CAPACITY OF ALLOY METAL IN REACTION ZONE	BTU/LM F	LI00980
C	CP1	USED TO CALCULATE CP CHANGE OF ALLOY METAL	BTU/LB R	LI00990
C	CP2	USED TO CALCULATE CP CHANGE OF ALLOY METAL	BTU/LB	LI01000
C	CPSTL	HEAT CAPACITY OF STEEL LINER	(BTU/LB-DEG F)	LI01010
C	CPWA	SPEC. HEAT OF WATER VAPOR	BTU/LB.-DEG. F	LI01020
C	CF	THERMAL IMPEDANCE BETWEEN BREEDER ELEMENTS	IN INNER ELEMENT	LI01030
C	CT	THERMAL IMPEDANCE BETWEEN BREEDER ELEMENTS	IN OUTER ELEMENT	LI01040
C	DELH	STANDARD HEAT OF HYDROLYSIS OF BREEDER	BTU/LB MOLE	LI01050
C	DELOUT	OUT TIME STEP		LI01060

C	DELTA	INTEGRATION TIME STEP	SEC.	LIT01070
C	DFILM	LITHIUM VAPOR FILM THICKNESS	FT	LIT01080
C	DIFF	DIFFUSION COEFF. TO COMB. ZONE	FT2/SEC.	LIT01090
C	DIFFLI	LITHIUM VAPOR DIFFUSION COEFFICIENT	FT2/SEC	LIT01100
C	DPROD	ENTHALPY CHANGE OF REACTION PRODUCTS IN REACTION ZONE	BTU/SEC	LIT01110
C	DP1,DP2,DP3	PSIA INCREASE IN CONTAINMENT PRESSURE DUE TO EACH	LIT01120	
C	DREAC	ENTHALPY CHANGE OF REACTANTS IN REACTION ZONE	LIT01130	
C	DT1	POOL TIME STEP (TEMP./RATE OF CHANGE OF TEMP.)	LIT01140	
C	DT2	CONT. GAS TIME STEP	LIT01150	
C	DT3	STEEL WALL TIME STEP	LIT01160	
C	DT4	COMBUSTION RATE TIME STEP	LIT01170	
C	DT5	COMBUSTION ZONE TEMP. TIME STEP	LIT01180	
C	DIBDT(I)	CONC. FLOOR TEMP. RATE OF CHANGE, NODE I	DEG. F/SEC.	LIT01190
C	DICDT(I)	CONC. WALL TEMP. RATE OF CHANGE, NODE I	DEG. F/SEC.	LIT01200
C	DIMIN	MINIMUM TIME STEP TO BE USED	SEC.	LIT01210
C	DT1,...,DT4	USED IN CALCULATING TIME STEP	SEC.	LIT01220
C	DYNAMI	SUBROUTINE USED IN CONTROLLING INTEGRATION LOOPS	LIT01230	
C	D1,D2	KINEMATIC VISCOSITY OF CELL GAS (SQUARED)	FT4/SEC2	LIT01240
C	EFILM	FILM DEPTH OF DEPLETED ZONE ABOVE COMB. ZONE (IN INCH)	LIT01250	
C	EMCONC	THERMAL EMISSIVITY OF CONCRETE	LIT01260	
C	EMG	THERMAL EMISSIVITY OF COMBUSTION ZONE	LIT01270	
C	EMINS	THERMAL EMISSIVITY OF CELL GAS	LIT01280	
C	EMLI	THERMAL EMISSIVITY OF INSULATION AROUND PAN	LIT01290	
C	EMSTL	THERMAL EMISSIVITY OF LITHIUM POOL	LIT01300	
C	ESCR	HEAT REMOVAL RATE BY EMERGENCY SPACE COOLING	BTU/SEC	LIT01310
C	ESCTIN	TIME AFTER SPILL WHEN ESCR BEGINS	SEC	LIT01320
C	EXHSTR	RATE OF CONTAINMENT GAS EXHAUST	LB/SEC	LIT01330
C	EXHSTV	RATE OF CONTAINMENT GAS EXHAUST	FT3/SEC	LIT01340
C	EXX	USED IN CALC. MASS & HEAT TRANSF. COEFF.	1/FT3	LIT01350
C	EX1,EX2	USED IN CALCULATING MASS & HEAT TRANSF. COEFF.	1/FT	LIT01360
C	FC11,FC2,FC3	FRACTION OF NITROGEN PRESENT IN EACH INJECTION	LIT01370	
C	FF1,FF2	USED IN HEAT BALANCE EQS. FOR SPRAY FIRE	BTU	LIT01380
C	FMLEAK	FRACT. OF MASS LEAKED OUT OF CONTAINMENT	LIT01390	
C	FMLEFT	FRACTION OF MASS STILL WITHIN CONTAINMENT	LIT01400	
C	FNI	WT. FRACTION OF NITROGEN IN CELL GAS	LIT01410	
C	FOUT	LOSS RATE OF CONT. GAS WHICH EITHER LEAKS OR IS EXHAUSTED	LIT01420	
C	FOX	WT. FRACTION OF OXYGEN IN CELL GAS	LIT01430	
C	FRA	FRACTION OF COMBUSTION PRODUCTS EVOLVED INTO CELL GAS	LIT01440	
C	FVA	WT. FRACTION OF WATER VAPOR IN CELL GAS	LIT01450	
C	G	AIR GAP BETWEEN STEEL LINER AND CONCRETE FLOOR	FT.	LIT01460
C		(INPUT AS INCHES)		LIT01470
C	GIN	GRAVITATIONAL CONSTANT	32.2 FT/SEC2	LIT01480
C	H	INTERIOR FILM COEF.	BTU/SEC-FT**2-DEG. F	LIT01490
C	HA	EXTERIOR FILM COEF.	BTU/SEC. FT**2 DEG. F	LIT01500
C		(INPUT AS BTU/HR FT**2 DEG F		LIT01510
C	HB	HEAT TRANSFER COEFFICIENT TO POOL	BTU/SEC-FT2-DEG F	LIT01520
C	HBINF	EQUILIBRIUM VALUE OF HB	LIT01530	
C	HCO	HEAT TRANSFER COEFFICIENT OF BOILING WATER	BTU/SEC-FT2	LIT01540
C	HF	GAS TRANSPORT COEFF. TO POOL	FT/SEC.	LIT01550
C	HFINF	EQUILIBRIUM VALUE OF HF	LIT01560	
C	HIN	COEFFICIENT FOR HEAT TRANSFER CORRELATIONS (H. HB. HF)	LIT01570	
C	HTCAPG	HEAT CAPACITY OF CONTAINMENT ATMOSPHERE	BTU/DEG.F	LIT01580
C				LIT01590

C	I	GENERAL PURPOSE DO LOOP INDEX	LIT01600
C	IB	DO LOOP INDEX USED FOR FLOOR CONCRETE ITERATIONS	LIT01610
C	INIT	INITIALIZING SUBROUTINE FOR INTEGRATION CALCULATIONS	LIT01620
C	INJEC1, INJEC2, INJEC3	FLAGS FOR GAS INJECTION ... INJEC=1 INDICATES THAT THE PARTICULAR INJECTION HAS OCCURRED	LIT01630
C	INTGRL	ARITHMETIC STATEMENT FUNCTION FOR FINDING INTEGRALS	LIT01640
C	J1=1	IF LITHIUM IS BREEDER	LIT01650
C	J2=1	IF HYDROGEN IS EVOLVED	LIT01660
C	K	LEAK RATE CONSTANT FROM CONTAINMENT 2.588E-09	LIT01670
C	KCON	THERMAL CONDUCTIVITY OF THE FLOOR AND WALL CONCRETE	LIT01680
C	KGAP	THERMAL COND. OF THE AIR GAP BETWEEN THE LINER AND CONCRETE	LIT01690
C	KFILM	THERM. COND. OF LI POOL/COMB. ZONE FILM BTU/SEC-FT-F	LIT01700
C	KINI	THERMAL CONDUCTIVITY OF INNER INSULATION - CALC. IN PROGLIT01720	LIT01710
C	KIN2	THERMAL CONDUCTIVITY OF OUTER INSULATION - CALC. IN PROGLIT01730	LIT01720
C	KPAN	THERMAL CONDUCTIVITY OF LI PAN 8BTU/HR-FT-DEG F	LIT01740
C	KSTL	THERMAL CONDUCTIVITY OF THE STEEL LINER (BTU/HR-FT-DEG F)	LIT01750
C	L	CONCRETE WALL ELEMENT THICKNESS FT.	LIT01760
C	LBN	DISTANCE BETWEEN TWO BREEDER ELEMENTS	LIT01770
C	LEAK	CELL GAS LEAKAGE RATE FROM CONTAINMENT 1/SEC.	LIT01780
C	LEAKO	INITIAL CELL GAS LEAKAGE RATE FROM CONTAINMENT 1/SEC.	LIT01790
C	LBP	LITHIUM BURNED IN POOL FIRE LB.	LIT01800
C	LIC	MASS OF LITHIUM IN CONTAINMENT LB.	LIT01810
C	LIL	AMOUNT OF LI LEFT IN POOL, BUT NOT ALLOWED TO BE LES	LIT01820
C	LILP	TRUE AMOUNT OF LITHIUM IN POOL LB.	LIT01830
C	LIS	THAN LIT/10 FOR NUMERICAL STABILITY IN HEAT TRANSFER	LIT01840
C	LIT	LI THIUM USED IN SPRAY FIRE LB.	LIT01850
C	LI	MASS OF LITHIUM IN POOL INITIALLY LB.	LIT01860
C	MA	CONCRETE FLOOR ELEMENT THICKNESS FT.	LIT01870
C	MAI	WT. OF INERT GAS IN CELL LB.	LIT01880
C	MAIR	WT. OF CELL GAS LB.	LIT01890
C	MB	MASS OF BREEDER ELEMENT LB MOLE	LIT01900
C	MCZ	REACTION ZONE MASS LB MOLES	LIT01910
C	MCZ1	INITIAL REACTION ZONE MASS LB MOLE	LIT01920
C	MH2	WT. OF HYDROGEN IN CONT. CELL GAS LB.	LIT01930
C	MLIH	WT. OF LITHIUM HYDROXIDE IN CONT. CELL GAS LB.	LIT01940
C	MLIN	WT. OF LITHIUM NITRIDE IN CONT. GAS CELL LB.	LIT01950
C	MLINI	MASS OF LITHIUM NITRIDE IN CONT. INITIALLY LB.	LIT01960
C	MLIO	WEIGHT OF LITHIUM OXIDE IN CELL GAS. PRESENTLY ALL OF THE	LIT01970
C		SPRAY FIRE PRODUCT REMAINS IN THE CELL GAS. A FRACTION	LIT01980
C		OF THE PRODUCTS FROM THE POOL FIRE IS ADDED LB.	LIT01990
C	MLIO1	MASS OF LITHIUM OXIDE IN CONT. INITIALLY LB.	LIT02000
C	MLIOH	MASS OF LI OH PRODUCT IN LB MOLES	LIT02010
C	MNI	WEIGHT OF NITROGEN IN CONTAINMENT CELL GAS LB.	LIT02020
C	MNI1	INITIAL WEIGHT OF NITROGEN IN CONTAINMENT LB.	LIT02030
C	MNIINJ	RATE OF INJECTION OF NITROGEN DURING A 60 SEC INTERVAL	LIT02040
C		USED TO MODEL HEDL PROCEDURE (LB/SEC)	LIT02050
C	MNINJ1, MNINJ2, MNINJ3	MASS OF NITROGEN INJECTED (LBS)	LIT02060
C	MOX	WEIGHT OF OXYGEN IN CELL GAS LB.	LIT02070
C	MOXI	INITIAL WEIGHT OF OXYGEN IN CONTAINMENT LB.	LIT02080
C	MOXINJ	RATE OF INJECTION OF OXYGEN USED TO MODEL HEDL EXPERIMENT	LIT02090
C		PROCEDURE. OCCURS DURING A 60 SEC. INTERVAL (LB./SEC)	LIT02100
C		MASS OF OXYGEN INJECTED (LBS.)	LIT02110
C	MOINJ1, MOINJ2, MOINJ3		LIT02120

C MPB MASS OF ALLOY METAL PRODUCT IN LB MOLES LIT02130  
C MWA WEIGHT OF WAT. VAP. IN CONTAINMENT CELL GAS LIT02140  
C MWAI MASS OF WATER VAPOR IN CONT. CELL GAS INITIALLY LB. LIT02150  
C NA NUMBER OF ELEMENTS IN BREEDER ZONE LIT02160  
C NAME(I) INPUT CONTAINING PROGRAM TITLE AND HEADING LIT02170  
C NL = NUMBER OF CONCRETE WALL NODES LIT02180  
C NLI = NUMBER OF CONCRETE FLOOR NODES LIT02190  
C NLI1 = NUMBER OF CONCRETE FLOOR NODES LIT02200  
C NLI1.NLI1M1 WALL AND FLOOR CONCRETE NUMBER OF NODES MINUS ONE LIT02210  
C NT NUMBER OF COOLANT TUBES DAMAGED LIT02220  
C OUTFIT LEAK FRACTION LIT02230  
C OVERP CONTAINMENT OVER PRESSURE PSIG LIT02240  
C OXLB OXYGEN BURNED LB. LIT02250  
C OXLB1 OXYGEN BURNED INITIALLY LB. LIT02260  
C OXLF5 OXYGEN LEFT AFTER SPRAY FIRE LB. LIT02270  
C PA GAS PRESSURE IN CELL PSIA LIT02280  
C PAZERO INITIAL CELL PRESSURE PSIA LIT02290  
C PBMELT MELTING POINT OF ALLOY METAL R LIT02300  
C PERCENT PERCENTAGE BY NUMBER OF PEROXIDE (VS. MONOXIDE) FORMED LIT02310  
C COMBUSTION LIT02320  
C PLIV PARTIAL PRESSURE OF LITHIUM VAPOR PSIA LIT02330  
C PZERO CONTAINMENT PRESSURE AFTER SPRAY FIRE LIT02340  
C OC FORCED CONVECTIVE COOLING HEAT FLOW LIT02350  
C QCN HEAT OF COMB. FOR NITROGEN REACTION BTU/LB. LI LIT02360  
C QCO HEAT OF COMBUSTION FOR OXYGEN REACTION BTU/LB. LI LIT02370  
C QCO1 HEAT OF COMBUSTION FOR MONOXIDE REACTION BTU/LB. LI LIT02380  
C QCO2 HEAT OF COMBUSTION FOR PEROXIDE REACTION BTU/LB. LI LIT02390  
C QCW HEAT OF COMB. FOR REACTION WITH WATER VAPOR BTU/LB. LI LIT02400  
C QIN HEAT ADDITION TO CELL GAS FROM SPRAY FIRE BTU LIT02410  
C QLIQH HEAT OF MELTING FOR LIQH BTU/LB-MOLE LIT02420  
C QMELT HEAT OF FUSION OF BREEDER BTU/LB MOLE LIT02430  
C QMELTP HEAT OF FUSION OF ALLOY METAL BTU/LB MOLE LIT02440  
C QOUT1,2,3,4 USED IN HEAT BALANCE EQS. FOR SPRAY FIRE BTU LIT02450  
C QRAD INDICATES A RADIATIVE HEAT FLOW BTU/SEC LIT02460  
C QRAD FROM STEEL FLOOR (PAN) TO FLOOR CONC. OR TO AMBIENT LIT02470  
C QRADCB FROM STEEL WALL TO WALL CONCRETE OR TO AMBIENT LIT02480  
C QRADCG FROM SPILL PAN TO CELL GAS LIT02490  
C QRADG FROM LI POOL TO GAS (NO COMB.) OR FROM COMB ZONE TO CELL LIT02500  
C QRADGP FROM COMB. ZONE TO LITHIUM POOL (COMB. ZONE MODEL ONLY) LIT02510  
C QRADS FROM SPILL PAN TO STEEL FLOOR LIT02520  
C QRADW FROM COMB ZONE TO WALL STEEL OR FROM LI POOL TO WALL STEEL LIT02530  
C QVAP HEAT OF VAPORIZATION OF LITHIUM BTU/LB LIT02540  
C QVA HEAT OF REACTION OF BREEDER WITH WATER LIT02550  
C QVAREA SURFACE AREA OF REACTION ZONE LIT02560  
C RAREA THE SYMBOL "R" DESIGNATES A TEMPERATURE RATE OF CHANGE IN SOME NODE LIT02570  
C TO RADIATION HEAT TRANSFER BETWEEN THAT NODE AND SOME OTHER NODE LIT02580  
C RADB IN FLOOR STEEL DUE TO RAD. TO FLOOR CONC. OR TO AMBIENT LIT02590  
C RADCB IN WALL STEEL DUE TO RAD. TO CONCRETE OR TO AMBIENT LIT02600  
C RADCC IN FLOOR CONCRETE FROM STEEL FLOOR (PAN) LIT02610  
C RADCC IN WALL CONCRETE FROM STEEL WALL LIT02620  
C RCZG IN GAS FROM COMBUSTION ZONE LIT02630  
C RCZP IN LITHIUM POOL FROM COMBUSTION ZONE LIT02640  
C RCZW IN WALL STEEL FROM COMBUSTION ZONE LIT02650  
C RGASPA IN PAN DUE TO RAD. TO CONTAINMENT GAS

C	RGLI	IN POOL DUE TO RAD. TO GAS (NO COMB)	LIT02660
C	RLIG	IN GAS DUE TO RAD. FROM POOL (NO COMBUSTION)	LIT02670
C	RLIW	IN WALL STEEL FROM LITHIUM POOL (NO COMB)	LIT02680
C	RPAGAS	IN CELL GAS DUE TO RAD. FROM LI PAN	LIT02690
C	RSPANST	IN WALL STEEL DUE TO RAD. FROM LITHIUM PAN	LIT02700
C	RSTPAN	IN PAN DUE TO RAD. TO FLOOR STEEL	LIT02710
C	RWLI	IN LITHIUM POOL FROM RAD. TO WALL STEEL (NO COMB)	LIT02720
C	RA	MEAN RADIUS OF COMBUSTION PRODUCT PARTICLES MICRONS	LIT02730
C	RCMBH2	STOICH. COMB. RATIO FOR H2O VAPOR REACT. LB. LI/LB. N	LIT02740
C	RCMBN	STOICH. COMB. RATIO OF NITROGEN REACT. LB. LI / LB. N	LIT02750
C	RCMBO	STOICH. COMB. RATIO FOR OXYGEN REACTION LB. LI/LB. O	LIT02760
C	RCMBO1	STOICH. COMB. RATIO FOR MONOXIDE REACTION LB. LI/LB. O	OLIT02770
C	RCMBO2	STOICH. COMB. RATIO FOR PEROXIDE REACTION LB. LI/LB. O	OLIT02780
C	RCMBW	STOICH. COMB. RATIO FOR WAT. VAP. REACT. LB. LI/LB. H2O	LIT02790
C	RELERR	MAXIMUM ALLOWABLE FRACTIONAL TEMP. CHANGE ACROSS A SINGLE INTEGRATION STEP. USED TO VARY TIME STEP.	LIT02800
C	RHCON	DENSITY OF FLOOR AND WALL CONCRETE	LIT02810
C	RHLI	DENSITY OF LITHIUM LB. / FT3	LIT02820
C	RHOA	DENSITY CELL GAS LB/FT3	LIT02840
C	RHOAI	INITIAL DENSITY OF CELL GAS LB/FT3	LIT02850
C	RHOLIH	DENSITY OF LITHIUM HYDROXIDE LB/FT3	LIT02860
C	RHOLIN	DENSITY OF LITHIUM NITRIDE LB/FT3	LIT02870
C	RHOLIO	DENSITY OF LITHIUM OXIDE LB/FT3	LIT02880
C	RHOLIV	LITHIUM VAPOR DENSITY ABOVE POOL LB/FT3	LIT02890
C	RHPAN	DENSITY OF LI SPILL PAN LBS/FT**3	LIT02900
C	RHPB	DENSITY OF ALLOY METAL LB-MOLE/FT3	LIT02910
C	RHSTL	DENSITY OF STEEL LINER (LB/FT3)	LIT02920
C	RIFCZG	RADIATIVE INTERCHANGE FACTOR BETWEEN COMB. ZONE AND THE CELL GAS	LIT02930
C	RIFCZP	RADIATIVE INTERCHANGE FACTOR BETWEEN COMB. ZONE AND THE POOL SURFACE	LIT02940
C	RIFCZW	RADIATIVE INTERCHANGE FACTOR BETWEEN COMB. ZONE AND CONTAINMENT WALLS	LIT02950
C	RIFPAG	RADIATIVE INTERCHANGE FACTOR - PAN TO GAS	LIT02960
C	RIFPAS	RADIATIVE INTERCHANGE FACTOR - PAN TO STEEL FLOOR	LIT02970
C	RIFPG	RAD. INT. FAC. BETWEEN POOL AND CELL GAS	LIT02980
C	RIFPW	RAD. INT. FACT. BETWEEN POOL AND WALL	LIT03000
C	RIFSLC	RADIATIVE INTERCHANGE FACTOR BETWEEN STEEL LINER AND CONCRETE SURFACE	LIT03010
C	RIN	UNIVERSAL GAS CONSTANT 1545 FT. LBF./LB.-DEG. F	LIT03020
C	RN1B	RATE OF NITROGEN CONSUMPTION LB./ SEC	LIT03030
C	RN2	DEGREE TO WHICH NITROGEN-LI REACTION OCCURS. VALUE IS BETWEEN ZERO AND ONE (=0 FOR NO REACTION, =1 FOR COMPLETE)	LIT03040
C	ROXLB	RATE OF OXYGEN CONSUMPTION BY POOL FIRE LB./SEC.	LIT03050
C	RRAD	INITIAL RADIUS OF REACTION ZONE FT	LIT03060
C	RTL1,RTG,RADB,RADW,RADCB,RADCW	VARIOUS RATES OF TEMP. CHANGE OF NODES DEG. F/SEC.	LIT03070
C	RVOL	INITIAL REACTION ZONE VOLUME FT3	LIT03080
C	RVOL1	REACTION ZONE VOLUME FT3	LIT03090
C	RVALB	RATE OF WATER VAPOR CONSUMPTION LB./SEC	LIT03100
C	RWCZ,RCZW,RCZG,RADB,RADW,RADCB,RADCW,RLIW,RWLI,RGLI,RLIG	VARIOUS RATES OF TEMP. CHANGE OF NODES DEG. F/SEC	LIT03110
C	R1	COEFFICIENT OF BREEDER IN WATER REACTION EQUATION	LIT03120

C	R2	COEFFICIENT OF ALLOY METAL IN WATER REACTION EQUATION	LIT03190
C	C	HEAT REMOVAL RATE BY EMERGENCY COOLING OF STEEL	LIT03200
C	C	FLOOR LINER BTU/SEC	LIT03210
C	C	TIME AFTER SPILL WHEN SFCLR BEGINS. SEC	LIT03220
C	C	SIGMA STEPHAN-BOLTZMAN CONSTANT ... .1713E-8 BTU/FT**2/HR/R**	LIT03230
C	C	SPILL TOTAL WEIGHT OF LITHIUM SPILLED LB.	LIT03240
C	C	WEIGHT FRACTION OF LITHIUM CONSUMED IN THE SPRAY FIRE	LIT03250
C	C	AMBIENT TEMPERATURE DEG. F	LIT03260
C	C	TAU TIME CONSTANT FOR TRANSIENT NATURAL CONVECTION	LIT03270
C	C	TWO THREES TIME IN SECONDS AT WHICH EACH INJECTION OCCUL	LIT03280
C	C	TEMP. OF ITH NODE OF CONCRETE FLOOR DEG. R	LIT03290
C	C	TBIC(I) INITIAL TEMP. OF ITH NODE OF CONCRETE FLOOR DEG. R	LIT03300
C	C	TBF, TCF, TGF, ETC. CORRESPONDING TEMP. IN DEGREES FAHRENHEIT	LIT03310
C	C	TBLOW INERT GAS INLET TEMP. DEG. R	LIT03320
C	C	TEMP. OF ITH NODE OF CONCRETE WALL DEG. R	LIT03330
C	C	TCIC(I) INITIAL TEMP. OF ITH NODE OF CONCRETE WALL DEG. R	LIT03340
C	C	COMBUSTION ZONE TEMPERATURE DEG R	LIT03350
C	C	TCZF COMBUSTION ZONE TEMP. IN FAHRENHEIT	LIT03360
C	C	TCZI INITIAL VALUE OF COMB. ZONE TEMP. DEG R	LIT03370
C	C	TE EQUILIBRIUM TEMP. RESULTING FROM SPRAY FIRE DEG. R	LIT03380
C	C	TTEFF NORMALIZED TEMP. OF LI POOL/COMB. ZONE FILM	LIT03390
C	C	TG GAS TEMP. AFTER SPRAY FIRE DEG. R	LIT03400
C	C	TGF CONTAINMENT GAS TEMP. IN FAHRENHEIT	LIT03410
C	C	TGZERO INITIAL CELL GAS TEMP. DEG. R	LIT03420
C	C	THF, THW CONCRETE FLOOR AND WALL THICKNESSES	LIT03430
C	C	INPUT AS INCHES, USED IN FI. FOR PROGRAM	LIT03440
C	C	THKIN1 INNER INSULATION THICKNESS INPUT AS INCHES	LIT03450
C	C	THKIN2 OUTER INSULATION THICKNESS INPUT AS INCHES	LIT03460
C	C	THKPAN SPILL PAN THICKNESS IN FEET (INPUT AS INCHES)	LIT03470
C	C	TIME TIME AFTER SPILL HAS OCCURRED SEC.	LIT03480
C	C	TIMEF STOP INTEGRATION TIME SEC.	LIT03490
C	C	TIMEO OUTPUT TIME INDICATOR SEC.	LIT03500
C	C	TINS1 TEMP. OF INNER NODE OF INSULATION DEG R	LIT03510
C	C	TINS2 TEMP. OF OUTER NODE OF INSULATION DEG R	LIT03520
C	C	TLI LITHIUM TEMP. IN POOL DEG. R	LIT03530
C	C	TLIF LITHIUM POOL TEMP. IN FAHRENHEIT	LIT03540
C	C	TLII INITIAL LITHIUM POOL TEMP. (DEG R)	LIT03550
C	C	TLIO INITIAL LITHIUM POOL TEMP. DEG. R	LIT03570
C	C	TN MELTING TEMP. OF BREEDER ZONE ELEMENT R	LIT03580
C	C	TO TEMP. OF CELL GAS AFTER SPRAY FIRE DEG. R	LIT03590
C	C	TPAN LITHIUM PAN TEMP (DEG R) SUSP PAN OPTION	LIT03600
C	C	TPANF LITHIUM PAN TEMP (DEG F)	LIT03610
C	C	TPANZO INITIAL PAN TEMPERATURE IN DEGREES R	LIT03620
C	C	TS STEEL WALL LINER TEMP. DEG. R	LIT03630
C	C	TSB STEEL FLOOR LINER TEMP. DEG. R	LIT03640
C	C	TSBF FLOOR STEEL LINER TEMPERATURE IN DEGREES FAHRENHEIT	LIT03650
C	C	TSBI INITIAL STEEL FLOOR LINER TEMP. DEG. R	LIT03660
C	C	TSF WALL STEEL LINER TEMPERATURE IN FAHRENHEIT	LIT03670
C	C	TSZERO INITIAL STEEL WALL LINER TEMP. DEG. R	LIT03680
C	C	TVAP BOILING POINT OF LITHIUM DEG. R	LIT03690
C	C	T1 FILM TEMP. BETWEEN CELL GAS AND POOL DEG. R	LIT03700
C	C	T2 FILM TEMP. BETWEEN CELL GAS AND STEEL WALL LINER DEG. R	LIT03710



C USUBA HEAT TRANSF. COEFF., CONTAINMENT-AMBIENT BTU/SEC-FT2-DEGLII03720  
 C V CELL FREE VOLUME FT3 LIT03730  
 C VOL VOLUME OF BREEDER ELEMENT LIT03740  
 C W THICKNESS OF STEEL POOL LINER FT. LIT03750  
 C (INPUT AS INCHES) LIT03760  
 C WA WT. FRACTION OF INERT GAS IN ATMOSPHERE LIT03770  
 C WAB WT. FRACTION OF INERT GAS IN FLOODING GAS LIT03780  
 C WN2 WEIGHT FRACTION OF NITROGEN IN ATMOSPHERE LIT03790  
 C WN2B WEIGHT FRACTION OF NITROGEN IN FLOODING GAS LIT03800  
 C W02 WEIGHT FRACTION OF OXYGEN IN ATMOSPHERE LIT03810  
 C W02B WEIGHT FRACTION OF OXYGEN IN FLOODING GAS LIT03820  
 C WWA WT. FRACTION OF WATER VAPOR IN FLOODING GAS LIT03830  
 C WWAB WT. FRACTION OF WATER VAPOR IN FLOODING GAS LIT03840  
 C XBLOW USED IN CONJUNCTION WITH ISFC LIT03850  
 C XESC USED IN CONJUNCTION WITH IESC LIT03860  
 C XMAIR AMOUNT OF GAS IN CONTAINMENT AFTER SPRAY LB.-MOLES LIT03870  
 C XLI WEIGHT FRACTION OF LITHIUM IN LIPB ALLOY LIT03880  
 C XPB WEIGHT FRACTION OF ALLOY METAL LIT03890  
 C XMOL MOL. WEIGHT OF CONTAINMENT GAS LB./LB.-MOLE LIT03900  
 C XMOLA MOLECULAR WT. OF INERT GAS LB./LB.-MOLE LIT03910  
 C XMOLAB MOL. WT. OF INERT FLOODING GAS LIT03920  
 C XSFL INDICATES EMERGENCY COOLING OF FLOOR STEEL LIT03930  
 C XSFL=0. FOR NO COOLING , XSFL=1. FOR COOLING LIT03940  
 C (1/SEC.) LIT03950  
 C XSFLC USED IN CONJUNCTION WITH ISFC LIT03960  
 C YALIC EFFECTIVE THERMAL ADMITTANCE, FILM-COMB. ZONE BTU/SEC-DLIT03970  
 C YALIG EFFECTIVE THERMAL ADMITTANCE, POOL-CELL GAS BTU/SEC-DEGLII03980  
 C YAPCZ EFFECTIVE THERMAL ADMITTANCE, POOL-COMB. ZONE BTU/SEC-DLIT03990  
 C ZLI THICKNESS OF LITHIUM NODE FT. LIT04000  
 C ZZ TEMPERATURE RATE OF CHANGE IN BREEDER ELEMENT LIT04010  
 C ZZ1 POOL TEMP. RATE OF CHANGE DEG. F/SEC. LIT04020  
 C ZZ2 LI SPILL PAN TEMP. RATE OF CHANGE (DEG R/SEC) LIT04030  
 C ZZ4 CELL GAS TEMP. RATE OF CHANGE DEG. F/SEC. LIT04040  
 C ZZ5 STEEL WALL LINER TEMP. RATE OF CHANGE DEG. F/SEC. LIT04050  
 C ZZ6 COMB. ZONE TEMP. RATE OF CHANGE DEG. F/SEC. LIT04060  
 C ZZ7 FLOOR STRUCTURE TEMP. RATE OF CHANGE DEG. F/SEC. LIT04070  
 C ZZ8 INNER INSULATION TEMP. RATE OF CHANGE DEG. F/SEC. LIT04080  
 C ZZ9 OUTER INSULATION TEMP. RATE OF CHANGE (SUSP. PAN OPTION) LIT04090  
 C ZZ99 USED TO ENSURE POSITIVE COMBUSTION RATE LIT04100  
 C PROGRAM DECISION FLAGS LIT04110  
 C IBLOW = 1 FLOOD CONTAINMENT WITH INERT GAS. LIT04120  
 C = 0 NO CONTAINMENT FLOODING. LIT04130  
 C ICMB = 0 NO OXYGEN LEFT AFTER SPRAY FIRE. LIT04140  
 C = 1 THERE IS STILL OXYGEN LEFT AFTER SPRAY FIRE. LIT04150  
 C SET INITIALLY TO 1 AND THEN RESET TO 0 WHEN THE LIT04170  
 C PROGRAM CALCULATES THAT THE OXYGEN HAS RUN OUT. LIT04180  
 C ICNI = 1 NITROGEN REACTIONS POSSIBLE. LIT04190  
 C = 0 NITROGEN REACTIONS NOT POSSIBLE. LIT04200  
 C ICZ = 1 COMBUSTION ZONE MODEL USED LIT04210  
 C = 0 COMBUSTION ZONE MODEL NOT USED LIT04220  
 C IESC = 1 EMERGENCY SPACE COOLING OPTION LIT04230  
 C LIT04240

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C = 0 NO EMERGENCY SPACE COOLING
C ILIT = 0 NO LITHIUM LEFT TO BURN.
C IMETH = 1 LITHIUM LEFT TO BURN (INITIAL CONDITION).
C IPAGE = 1 RUNGE-KUTTA METHOD OF INTEGRATION USED.
C ISFLC = 3 SIMPSON'S RULE METHOD OF INTEGRATION USED.
C IOPTB = 1 EMERGENCY COOLING OF STEEL FLOOR LINER OPTION
C IOPTB = 0 NO EMERGENCY COOLING OF STEEL FLOOR LINER
C FLAG = .TRUE. NO WALL CONCRETE
C FLAG1 = .TRUE. NO FLOOR CONCRETE
C FLAGJ = .TRUE. INJECTIONS OF DRY GAS DURING RUN
C FLAGL = .TRUE. LILP IS FIXED AT A MINIMUM
C FLAGSI = .TRUE. YES ON SUSPENDED PAN GEOMETRY
C IOPTB=1 IF INTERNAL BLANKET ACCIDENT OPTION IS TO BE USED

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0001 IMPLICIT REAL (K,L,M)
0002 DIMENSION TCF(20),TBF(20),TB(20),TC(20),DTCDT(20),DTBDT(20),
      TCIC(20),TBIC(20),NAME(100),L(20),LI(20),C4(20),C10(20),
      TN(20),RAD(20),ARE(20),VOL(20),CF(20),CT(20),Z2(20),
      TNF(20),QC(20),ATQ(20),ATI(20)
      LOGICAL FLAG,FLAG1,FLAGL,FLAGJ,FLAGSI,FLAGIO

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0004 REAL INTGRL
0005 REAL NT,MLI,MCZ,MLIOH,MLIO,MLIT,MLIJ
0006 REAL NA,LBN,LBR,LB2,MB(20)
0007 REAL J1,J2
0008 COMMON IMETH,ICOUNT,ISTORE,INOIN,IPASS,DELT,XIC(101),ZZZ(501)
0009 KPAN,RHPAN,CPAN,TPANZO,APAN,AWB,THKPAN,BREDTH,ASLI,SPILL,QCOI,
      QC02,QCN,QCM,QVAP,FLAGJ,FLAGL,FLAGIO,IBLOW,IESC,ISFLC,RHOLIN,
      RHOLIO,RHOLIH,CPA,CPLI,RHLI,AKLI,CPSTL,RHSTL,KSTL,CPCON,RHCON,
      KCON,PAZERO,TGZERO,TSZER,TSBI,TA,TLII,DPI,DP2,DP3,ESCR,SFLCR,
      CPAB,TBLOW,EXHSTV,BLOWV,TBF,TCF,THKIN2,THKIN1,AINS,CPINS,RHINS,
      IOPTB,NT,RRAD,AMLI,HCO,QLIOH,CPLIOH,PBMLT,CPI,CP2,RHPB,
      AMPB,XLI,CPLI,CPLI1,CPBBI,RI,R2,J1,J2,QMELT,QMELTP,DELH
      COMMON /EXTRA/ TINS2F,TB,TC,TG,TGF,TSB,TSBF,TS,TSF,TCZ,
      TCZF,TLI,TLIF,TPAN,TPANF,OVERP,MDX,MNI,LILP,HF,HB,EFILM,DFILM,
      TINS1,TINS2

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0010 C*****
      C INPUT SECTION
      C*****
      C***** READ IN TITLE AND HEADINGS *****

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0011 998 CONTINUE
0012 READ(5,707,END=999) (NAME(I),I=1,100)
0013 707 FORMAT(20A4)

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C ***** READ IN FLAGS AND OPTIONS *****
C READ (5,705) FLAG,FLAG1,FLAGJ,FLAGSI,IBLOW,IESC,ISFLC,IOPTB
C FORMAT (5(L1,1X),4(I1,1X))

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0014 C***** READ IN CONTAINMENT SPECIFICATIONS *****
0015 READ(5,702) AW,V,CH,W02,WWA,WA

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0016

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0017 READ(5,702) G,KGAP,W,K,EMGF,BETA
0018 READ(5,702) THW,THF,AWB
0019 READ(5,709) NL,(L(1),I=1,NL)
0020 READ(5,709) NL1,(L1(1),I=1,NL1)
0021 FORMAT(12,15F5.3)
0022 IF(FLAGS) READ(5,702) TPANZO,APAN, AINS,BREDOH
0023 IF(FLAGS) READ(5,702) THKPAN,THKIN1,THKIN2
0024 IF(FLAGS) READ(5,702) KPAN,RHPAN,CPAN,RHINS,CPINS,EMINS
0025 READ(5,702) TEHCZO,XMEHC,AEHC,CPEHC
C
C***** READ IN HEAT TRANSFER CORRELATION COEFFICIENTS *****
0026 READ(5,702) HIN,HINEHC,HINGS,HINSAM,TAUCZ
C
C***** READ IN SPILL PARAMETERS *****
0027 READ(5,702) ASLI,SPILL,SPRAY,FRA,RA,XMOLA
0028 702 FORMAT(6F12.4)
C
C***** READ IN REACTION CONSTANTS *****
0029 READ(5,702) QCO1,QCO2,QCN,QCN
0030 READ(5,702) RCMBO1,RCMBO2,RCMBN,RCMBW,RCMBH2
0031 READ(5,702) TMELT,TVAP,QVAP,EMCZ,TCZI,PERCEN
C
C***** READ IN PHYSICAL CONSTANTS *****
0032 READ(5,702) RHOLIO,RHOLIN,RHOLIH,CPA
0033 READ(5,702) CPLI,RHLI,AKLI,EMSTL,EMLI,EMCONC
0034 READ(5,702) CPSTL,RHSTL,KSTL,CPCON,RHCON,KCON
C
C ***** READ IN INITIAL CONDITIONS *****
0035 READ(5,702) PAZERO,TGZERO,TSZERO,TSBI,TA,TLII
C
C***** READ IN INTEGRATION CONTROL PARAMETERS *****
0036 READ(5,706) IMETH,DTMIN,TIMEF,RELERR,DELOUT
0037 706 FORMAT(14,5F12.4)
C
C***** READ IN INJECTION PARAMETERS *****
0038 IF(FLAGJ) READ(5,1030)TONE,DPI,FCT1,TTWO,DP2,FCT2,TTREE,DP3,FCT3
0039 1030 FORMAT(9F8.4)
C
C***** CONTAINMENT FLOODING WITH INERT GAS OPTION *****
0040 708 FORMAT(I4)
0041 IF(1BLOW.EQ.1) READ(5,702) W026,W0AB,W02B,W0LAB,CPAB,TBLOW,BLOWV,
LIT04780
LIT04790
LIT04800
LIT04810
LIT04820
LIT04830
LIT04840
LIT04850
LIT04860
LIT04870
LIT04880
LIT04890
LIT04900
LIT04910
LIT04920
LIT04930
LIT04940
LIT04950
LIT04960
LIT04970
LIT04980
LIT04990
LIT05000
LIT05010
LIT05020
LIT05030
LIT05040
LIT05050
LIT05060
LIT05070
LIT05080
LIT05090
LIT05100
LIT05110
LIT05120
LIT05130
LIT05140
LIT05150
LIT05160
LIT05170
LIT05180
LIT05190
LIT05200
LIT05210
LIT05220
LIT05230
LIT05240
LIT05250
LIT05260
LIT05270
LIT05280
LIT05290
LIT05300
EXHSTV,BLIN,BLOUT
XBLOW=0.
IF(1BLOW.EQ.1) GO TO 437
BLIN=0.
BLOUT=0.
W02B=0.
W0AB=0.
W02B=0.
W0AB=0.
W02B=0.
W0AB=0.
XMOLAB=1.
CPAB=1.

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```

0052 TBL0W=1.
0053 BLOW=0.
0054 EXHSTV=0.
0055
0056 437 CONTINUE
0057 WAB=1.-W02B-WN2B-WWAB
0058 BLOWR = 1.35E-03 * BLOWV
      EXHSTR = 1.35E-03 * EXHSTV
C
C***** EMERGENCY SPACE COOLING OF CONTAINMENT OPTION *****
0059 XESC=0.
0060 IF(IESC.EQ.1) READ(5,702) ESCR,ESCTIN
0061 IF(IESC.EQ.1) GO TO 439
0062 IF(ISFLC.EQ.1) READ(5,702) SFPCR,SFLTIN
0063 SFSL=0.
0064 SFPCR=0.
0065 ESCR= 0.
0066 ESCTIN=0.
C
0067 439 CONTINUE
0068 IF(ISFLC.EQ.1) GO TO 440
C***** EMERGENCY STEEL FLOOR LINER COOLING OPTION *****
0069 SFLTIN=0.
0070 440 CONTINUE
C
C***** INTERNAL BLANKET ACCIDENT OPTION *****
0071 IF (IOPTB .EQ. 1) READ (5,702) NT,RRAD,AMLI,HCO,QLIOH,CPLIOH
0072 IF (IOPTB .EQ. 1) READ (5,702) PBWELT,CP1,CP2,RHPB,AMPB,XLI
0073 IF (IOPTB .EQ. 1) READ (5,702) CPPL,CPLI1,CPPB1,R1,R2
0074 IF (IOPTB .EQ. 1) READ (5,702) J1,J2,OMELT,OMELTP,DELH
0075 IF (IOPTB .EQ. 1) GO TO 441
0076 NT=0.
0077 RRAD=0.
0078 AMLI=7.0
0079 HCO=1.
0080 QLIOH=0.
0081 CPLIOH=1.
0082 441 CONTINUE
C
C***** PRINT OUT THE INPUT *****
C
C*****
C
RCMBO=((100.-PERCEN)*RCMBO1+PERCEN*RCMBO2)/100.
QCO=((100.-PERCEN)*RCMBO1*QCO1+PERCEN*RCMBO2*QCO2)/(RCMBO*100.)
ZLI=SPILL/RHLI/ASLI
WRITE(6,802) (NAME(I),I=1,60)
FORMAT ('1',3(20X,20A4,/,/),/)
802 WRITE(6,142) CPLI,RHLI,RHOLIO,AKLI,EMLI,CPSTL,RHSTL,RHOLIN,KSTL,
      EMSTL,CPCON,RHCON,RHOLIN,KCON,EMCONC, KGAP,EMCZ
      WRITE(6,143) AM,V,THW,K,CH,W,THF,G
      WRITE(6,144) ASLI,SPILL,SPRAY,W02,ZLI
      WRITE(6,153) HIN,HINEHC,HINGS,HINSAM
      WRITE(6,145) QCO,RCMBO,TVAP,RCMBH2,PERCEN,QCN,RCMBN,TMELT,FRA,
0083
0084
0085
0086
0087
0088
0089
0090
0091
0092
0093
LIT05310
LIT05320
LIT05330
LIT05340
LIT05350
LIT05360
LIT05370
LIT05380
LIT05390
LIT05400
LIT05410
LIT05420
LIT05430
LIT05440
LIT05450
LIT05460
LIT05470
LIT05480
LIT05490
LIT05500
LIT05510
LIT05520
LIT05530
LIT05540
LIT05550
LIT05560
LIT05570
LIT05580
LIT05590
LIT05600
LIT05610
LIT05620
LIT05630
LIT05640
LIT05650
LIT05660
LIT05670
LIT05680
LIT05690
LIT05700
LIT05710
LIT05720
LIT05730
LIT05740
LIT05750
LIT05760
LIT05770
LIT05780
LIT05790
LIT05800
LIT05810
LIT05820
LIT05830

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0094 QCW,RCMBW,QVAP,RA
0095 WRITE(6,146) TZERO,TLII,TSBI,WA,PAZERO,TSZERO,TCZI,TA,WVA
0096 WRITE(6,147) IMETH,DTMIN,TIMEF,RELERR,DELOUT
0097 WRITE(6,148) IBLOW,IESC,ISFLC,FLAG,FLAG1,IOPTB
0098 WRITE(6,149) W02B,BLOWV,ESCR,SFLCR,CPA,WVAB,BLOUT,ESCTIN,SFLTIN,
    CPA,WN2B,BLIN,EXHSTV,TBLOW,XMOLA,XMOLAB
0099 IF(FLAGS) WRITE(6,151) TPANZO,APAN,AWB,THKPAN,BREATH,KPAN,RHPAN,
    CPPAN,EMINS
0100 IF(FLAGS) WRITE(6,152) THKINI,THKIN2,AINS,RHINS,CPINS
0101 WRITE(6,154) TEHCZO,XMEHC,AEHC,CPEHC
    IF (IOPTB.EQ.1) WRITE(6 1101) NI,RRAD,AMLI,HCD,OLIOH,CPLIOH,
    PMELI,CP1,CP2,RHPB,CP1PB,XLI,CPPL,CPL1,CP1PB,RI,R2,
    J1,J2,OMELT,OMELTP,DELH
0102 FORMAT(' PHYSICAL PROPERTIES'/IX,19(1H-)//T10,'CPLI = ',F12.4,
    T35,'RHLI = ',F12.4,T60,'RHOLIO = ',F12.4,T85,'AKLI = ',F12.4,
    T110,'EMLI = ',F12.4//T10,'CPSTL = ',F12.4,T35,'RHSTL = ',F12.4,
    T60,'RHOLIN = ',F12.4,T85,'KSTL = ',F12.4,T110,'EMSTL = ',F12.4//
    T10,'CPCON = ',F12.4,T35,'RHCON = ',F12.4,T60,'RHOLIH = ',F12.4,
    T85,'KCON = ',F12.4,T110,'EMCON = ',F12.4//
    T60,'KGAP = ',F12.4,T85,'EMCZ = ',F12.4//)
0103 FORMAT(' INNER CONTAINMENT DIMENSIONS'/IX,28(1H-)//T10,'AN = ',
    F12.4,T35,'V = ',F12.4,T60,'THW = ',F12.4,T85,'K = ',F12.4//T10,
    'CH = ',F12.4,T35,'W = ',F12.4,T60,'THF = ',F12.4,T85,'G = ',
    F12.4//)
0104 FORMAT(' SPILL PARAMETERS'/IX,16(1H-)//T10,'ASLI = ',F12.4,T35,
    'SPILL = ',F12.4,T60,'SPRAY = ',F12.4,T85,'W02 = ',F12.4,T110,
    'ZLI = ',F12.4//)
0105 FORMAT(' HEAT TRANSFER CORRELATION COEFFICIENTS'/IX,38(1H-)//T10,
    'HIN = ',F12.4,T35,'HINEHC = ',F12.4,T60,'HINGS = ',F12.4,
    T85,'HINSAM = ',F12.4//)
0106 FORMAT(' COMBUSTION PARAMETERS'/IX,21(1H-)//T10,'QCC = ',F12.4,
    T35,'RCMBO = ',F12.4,T60,'TVAP = ',F12.4,T85,'RCMBH2 = ',F12.4,
    T110,'PERCEN = ',F12.4//T10,'QCN = ',F12.4,T35,'RCMBN = ',F12.4,
    T60,'TMELT = ',F12.4,T85,'FRA = ',F12.4//T10,'QCV = ',F12.4,T35,
    'RCMBW = ',F12.4,T60,'QVAP = ',F12.4,T85,'RA = ',F12.4//)
0107 FORMAT(' INITIAL CONDITIONS'/IX,18(1H-)//T10,'TGZERO = ',F12.4,
    T35,'TLII = ',F12.4,T60,'TSBI = ',F12.4,T85,'WA = ',F12.4,T110,
    'PAZERO = ',F12.4//T10,'TSZERO = ',F12.4,T35,'TCZI = ',F12.4,T60,
    'TA = ',F12.4,T85,'WVA = ',F12.4//)
0108 FORMAT(' INTEGRATION CONTROL PARAMETERS'/IX,30(1H-)//T10,
    'IMETH = ',I4,T35,'DTMIN = ',F12.4,T60,'TIMEF = ',F12.4,T85,
    'RELERR = ',F12.4,T110,'DELOUT = ',F12.4//)
0109 FORMAT(' OPTIONS IN EFFECT'/IX,17(1H-)//T10,'IBLOW = ',I4,T35,
    'IESC = ',I4,T60,'ISFLC = ',I4,T85,'FLAG = ',I4,T110,'FLAG1 = ',
    I4//T10,'IOPTB = ',I4//)
0110 FORMAT(' MISCELLANEOUS INPUT'/IX,19(1H-)//T10,'W02B = ',F12.4,T35,
    'BLOWV = ',F12.4,T60,'ESCR = ',F12.4,T85,'SFLCR = ',F12.4,T110,
    'CPA = ',F12.4,T110,'WVAB = ',F12.4,T35,'BLOUT = ',F12.4,T60,
    'ESCTIN = ',F12.4,T85,'SFLTIN = ',F12.4,T110,'CPAB = ',F12.4//T10,
    'WN2B = ',F10.4,T30,'BLIN = ',F10.4,T50,'EXHSTV = ',F10.4,T70,
    'TBLOW = ',F10.4,T90,'XMOLA = ',F10.4,T110,'XMOLAB = ',F10.4)
0111 FORMAT(//,' DATA FOR SUSPENDED PAN OPTIONAL GEOMETRY: '//,IX,
    41(1H-)//T10,'TPANZO = ',F12.4,T35,'APAN = ',F12.4,T60,'AWB =

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      .F12.4,T85,'THKPN = ',F12.4,T110,'BREDTH = ',F12.4//T10,
      .KPN = ',F12.4,T35,'RHAN = ',F12.4,T60,'CPPAN = ',F12.4,T85,
      .EMINS = ',F12.4)
152  FORMAT(//T10,'THKIN1 = ',F12.4,T35,'THKIN2 = ',F12.4,T60,'AINS = ',
      .F12.4,T85,'RHINS = ',F12.4,T110,'CPINS = ',F12.4)
153  FORMAT (T60,'FLAGS = ',
      .L1,T85,'FLAG = ',L1,T110,'FLAGSI = ',L1//)
154  FORMAT(//,'EXTANEOUS HEAT CAPACITY NODE DATA'/IX,33(1H-)//T10,
      .T85,'J2 = ',F10.1,T110,'QHEC = ',F12.4,T35,'XMEHC = ',F12.4,T60,'AEHC = ',F12.4,
      .T85,'CPEHC = ',F12.4)
1101 FORMAT(' INTERNAL BLANKET OPTION INPUT'/IX,29(1H-)//T10,
      .NT = ',F10.1,T35,'RRAD = ',F10.2,T60,'AMLI = ',F10.2,
      .T85,'HCO = ',F10.2,T110,'QLIOH = ',F10.2//T10,'CPLIOH = ',F10.2,
      .T35,'PBMELT = ',F10.2,T60,'CPI = ',F10.3,T85,'CP2 = ',F10.5,
      .T110,'RHPB = ',F10.2//T10,'AMPB = ',F10.2,T35,'XLI = ',F10.3,
      .T60,'CPPL = ',F10.3,T85,'CPLI1 = ',F10.2,T110,'CPPB1 = ',F10.2//
      .T10,'R1 = ',F10.3,T35,'R2 = ',F10.3,T60,'J1 = ',F10.1,
      .T85,'J2 = ',F10.1,T110,'QMELT = ',F10.2//T10,'QMELTP = ',F10.2,
      .T110,'DELH = ',F10.1)
C
C*****
C INITIALIZE PROGRAM VARIABLES
C*****
C
EMF=0.9
GAMMA=1.4
FPG=1.
FPW=1.
IF (FLAGS)FPG=0.23
IF (FLAGS)FPW=0.384
C3=0.
C5=0.
C7=0.
C8=0.
C9=0.
CMRRI=0.
LIBP=0.
LILOX=0.
LILNI=0.
LEAKO=0.
MLIN=0.
MLINI=0.
MLIH=0.
MH2=0.
OXLB=0.
OXLB1=0.
HTCAPG=1.
OUTINT=0.
TIME=0.
RADCC=0.
RADCB=0.
RADB=0.
ZZZ=0.
0112
0113
0114
0115
LIT06370
LIT06380
LIT06390
LIT06400
LIT06410
LIT06420
LIT06430
LIT06440
LIT06450
LIT06460
LIT06470
LIT06480
LIT06490
LIT06500
LIT06510
LIT06520
LIT06530
LIT06540
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LIT06580
LIT06590
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LIT06650
LIT06660
LIT06670
LIT06680
LIT06690
LIT06700
LIT06710
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LIT06770
LIT06780
LIT06790
LIT06800
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LIT06820
LIT06830
LIT06840
LIT06850
LIT06860
LIT06870
LIT06880
LIT06890

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0145 ZB=0.
0146 ZG=0.
0147 ZG6=0.
0148 CMBRO=0.
0149 CMBRN=0.
0150 CMBRW=0.
0151 RXLB=0.
0152 RWALB=0.
0153 IG=0
0154 J=IOP TB
0155 XPB=1.-XLI
0156 CGZ=0.
0157
0158 MLIY=0.
0159 MLIQH=0.
0160 RVOL=4.189*RRAD*3
0161 MCZ1=RVOL/(AMLI/RHLI)
0162 MLI1=625.87*RHLI/AMLI-MCZ1
0163 MLIIT=0.
0164 HA=1.
0165 H=1.
0166 NN=8
0167 NA=8.
0168 ND=NN-1
0169 DO 31 J=1,NN
0170 TN(J)=TLII
0171 ZZ(J)=0.
0172 ZZ(1)=1.
0173 ZZ1=1.
0174 CPLI=CPLI*AMLI
0175 CPMLI=CPLI
0176 CPPZ=1.
0177 DO 185 IAM=1,20
0178 C4(IAM)=0.
0179 C10(IAM)=0.
0180 DTCDT(IAM)=0.
0181 DTBDT(IAM)=0.
0182 IF(FLAGSI) CALL SI
0183 DELT=DTMIN
0184 HF=0.
0185 HB=0.
0186 RCMBO=((100.-PERCEN)*RCMBD1+PERCEN*RCMBD2)/100.
0187 QCO=((100.-PERCEN)*RCMBD1+QCO1+PERCEN*RCMBD2+QC02)/(RCMBD+100.)
0188 FLAGIO=.FALSE.
0189 IF (.NOT. FLAGS) TPANZO=0.
0190 TPAN=TPANZO
0191 TINS1=0.5*(TPANZO+TGZERO)
0192 TINS2I=TGZERO
0193 TINS1=TINS1I
0194 TINS2=TINS2I
0195 TEHC=TEHCZO
0196 DFILM=0.
0197 INJEC1=0

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31

185

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0198 INJEC2=0
0199 INJEC3=0
0200 TAU=120.
0201 SIGMA=4.7611E-13
0202 IF (ILOPTB.EQ.1) SIGMA=0.
0203 NLM1=NL1-1
0204 NL1M1=NL1-1
0205 FLAG1=.FALSE.
0206 FLAGL=.FALSE.
0207 IF (ILOPTB.EQ.1) GO TO 25
0208 FLAG=.FALSE.
0209 IF (THW.LT. 0.01) FLAG=.TRUE.
0210 IF (THF.LT. 0.01) FLAG1=.TRUE.
0211 LIS=SPILL*SPRAY
0212 LIT=SPILL-LIS
0213 WN2=1.-W02-WWA-WA
0214 XMOL=1./((W02/32.+WN2/28.+WWA/18.+WA/XMOLA)
0215 RIN=1545./XMOL
0216 TIMEQ=-.001
0217 TLI=TLII
0218 LILP=LIT
0219 LIL=LILP
0220 ZLI=LILP/RHLI/ASLI
0221 TCZ=TCZI
0222 FMLEFT=1.0
0223 GIN=32.2
0224 TS=TSZERO
0225 TSB=TSBI
0226 DO 1001 I=1,NL
0227 TCIC(I)=TSZERO
0228 TC(I)=TSZERO
0229 L(I)=THW*L(I)/12.
0230 DO 1002 I=1,NL1
0231 TBIC(I)=TSBI
0232 TB(I)=TSBI
0233 L1(I)=THF*L1(I)/12.
0234 ICZ=1
0235 ICMB=1
0236 ILIT=1
0237 ICNI=1
0238 RHOA=PAZERO*144./RIN/TGZERO
0239 RHOAI=RHOA
0240 IPAGE=50
0241 MNII=WN2*RHOAI*V
0242 MNI=MNI
0243 MOXI=W02*RHOAI*V
0244 MLIOI=LIS*(1.+RCMBO)/RCMBO
0245 MWAI=WWA*RHOAI*V
0246 MAI=MVAI
0247 MAI=WA+RHOAI*V
0248 MA=MVAI
0249 LIC=LIS

```

25

1001

1002

C

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LI107430
LI107440
LI107450
LI107460
LI107470
LI107480
LI107490
LI107500
LI107510
LI107520
LI107530
LI107540
LI107550
LI107560
LI107570
LI107580
LI107590
LI107600
LI107610
LI107620
LI107630
LI107640
LI107650
LI107660
LI107670
LI107680
LI107690
LI107700
LI107710
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LI107840
LI107850
LI107860
LI107870
LI107880
LI107890
LI107900
LI107910
LI107920
LI107930
LI107940
LI107950

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0284 627 CONTINUE
0285 TE=TGZERO
0286 150 CONTINUE
0287 TG=TE
0288 MOX=MOXI-LIS/RCMBO
0289 MOXI=MOX
0290 MLIQ=MLIOI
0291 XMAIR=MNI/28.+MOX/32.+MA/XMOLA+MMA/18.
0292 PZERO=1545.*XMAIR*TG/144./V
0294 TGZERO=TG
0295 WRITE(6,726) TG,PZERO
0297 FORMAT(///) SPRAY FIRE RESULTS'/IX,18(1H-)//5X,'TGZERO = ',F6.1,
      ' PZERO = ',F6.3///)
0298 IF (FLAG)WRITE(6,1090)TONE,DP1,FCT1,TTWO,DP2,FCT2,ITHREE,DP3,FCT3
1090 FORMAT(//) GAS INJECTION DATA',/1X,18(1H-)//3(SX,'AT TIME = ',
      .F8.0,5X,'DELTA P = ',F8.4,5X,'FCT N2 = ',F8.4,./)//)
C*****
C SPRAY FIRE COMPUTATION CONCLUDED *****
C
0299 850 CALL INIT
C
C*****
C* START OF DYNAMIC CYCLE *
C* ----- *
C* START OF INTEGRATION CYCLE *
C*****
C
0300 200 CONTINUE
C ARTIFICIAL INJECTION OF OXYGEN AND NITROGEN
C TO MODEL HEDL EXPERIMENTAL PROCEDURE
0301 MOXINJ=0.
0302 MNIINJ=0.
0303 IF (.NOT. FLAG) GO TO 1060
0304 IF (TIME .LT. TONE .OR. TIME .GT. TONE+60.) GO TO 1040
0305 IF (INJEC1 .EQ. 0 .AND. DP1 .GT. 0.0) WRITE(6,1080) TONE,DP1
0306 FORMAT(//) INJECTION OF GAS AT TIME = ',F8.0,' TO RAISE PRESSURE
      'Y',F8.4,' PSI')
0307 INJEC1=1
0308 MOINJ1= 2.9822*V/TG+DP1*(1.-FCT1)
0309 MNIINJ1= 2.6094*V/TG+DP1*FCT1
0310 MOXINJ=MOINJ1/60.
0311 MNIINJ=MNIINJ1/60.
0312 IF (TIME .LT. TTWO .OR. TIME .GT. TTWO+60.) GO TO 1050
0313 IF (INJEC2 .EQ. 0 .AND. DP2 .GT. 0.0) WRITE(6,1080) TTWO,DP2
0314 INJEC2=1
0315 MOINJ2= 2.9822*V/TG+DP2*(1.-FCT2)
0316 MNIINJ2= 2.6094*V/TG+DP2*FCT2
0317 MOXINJ=MOINJ2/60.
0318 MNIINJ=MNIINJ2/60.
0319 IF (TIME .LT. TTHREE .OR. TIME .GT. TTHREE+60.) GO TO 1060
0320 IF (INJEC3 .EQ. 0 .AND. DP3 .GT. 0.0) WRITE(6,1080) TTHREE,DP3
0321 INJEC3=1
0322 MOINJ3= 2.9822*V/TG+DP3*(1.-FCT3)

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0323 MNINJ3= 2.6094*V/TG*DP3*FCT3
0324 MOXINJ=MOXINJ3/60.
0325 MNINJ=MOXINJ3/60.
0326 CONTINUE
0327 IF (IOPTB .EQ. 1) GO TO 21

C
C COMPUTE PHYSICAL PROPERTIES DEPENDENT ON TEMPERATURE
C CALCULATE AIR COMPOSITION AND SPECIFIC HEAT AT CONST. VOLUME **LIT09080
C
MAIR=MOX+MNI+MWA+MH2+MA
RHOA=MAIR/V
FDX=MOX/MAIR
FWA=MWA/MAIR
FNI=MNI/MAIR
CPMOX= (0.184 + 3.2E-06*TG - 1.36E04 / (TG**2))*MOX
CPMNI = (0.172 + 8.57E-06*TG + 1.02E-09*TG**2)*MNI
CPWA=0.44
CPH2=3.76
CPLH=0.67
CPN2=(0.172+8.57E-06*TG+1.02E-09*TG**2)
CPLIO=.0602*TG**326
CPLIN=.3368+3.67E-4*TG
CPLIO=CPLIO+MLIO
CPLZ=CPLI
AKLZ=AKLI
TLI=1216.
IF (J2 .EQ. 0.) GO TO 851
TLIK=(TLI-462.)/(1.8+273.
TCZK=(TCZ-462.)/(1.8+273.
CPPB=CPI+CP2+TLIK
CPPZ=CP1+CP2+TCZK
IF (TLI .GT. PBMELT) CPPB=CPPL
IF (TCZ .GT. PBMELT) CPPZ=CPPL
CPFAC=0.004938*TLI -6.20741
CPFAC=0.004938*TCZ -6.20741
CPFI=1.0037-.01063*CPFAC+.00564*CPFAC**2-.001279*CPFAC**3
IF (TCZ .GE. 1302.) GO TO 1255
CPLZ=1.0037-.01063*CPFAC+.00564*CPFAC**2-.001279*CPFAC**3
CPLI=XLI+CPLI+XPB+CPPB
CPLZ=XLI+CPLZ+XPB+CPPZ
CPLI=CPLI+AMLI
CPLZ=CPLZ+AMLI
IF (J1 .NE. 1.) GO TO 851
RHLI=33.49-.0035*(TLI -460.)
AKLI=(10.48+2.767E-03*(TLI -817.))-0.322E-06*(TLI -817.)**2/1488.
AKLZ=(10.48+2.767E-03*(TCZ -817.))-0.322E-06*(TCZ -817.)**2/1488.
IF (IOPTB .EQ. 1) GO TO 851
CPLI=((LIT-LIBP)*CPLI+LIXO+CPLIO+LILNI+CPLIN)/LILP
IF (TCZ .LT. TMELT) DREAC=19500.+8.2*(TCZ-672.)+CPLZ*(TCZ-537.)
**R1
IF (TCZ .GE. TMELT) DREAC=19500.+8.2*(TCZ-672.)+R1*CPLI+
.(TMELT-537.)+R1*QMELT+R1*CPLZ*(TCZ-TMELT)

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0370 HYD=J2+3.5*(TCZ-537.)
0371 LIOHL=(2.-J2)*12.5*(TCZ-537.)
0372 LIOHG=19070.+20.74*(TCZ-1338.)*2.(2.-J2)
0373 OML=CPPZ*(TCZ-537.)*R2
0374 OMG=R2*(CPPB1*(PBMELT-537.)+QMLTP+CPPZ*(TCZ-PBMELT))
0375 TEM1=AMINI(PBMELT,1338.)
0376 TEM2=AMAX1(PBMELT,1338.)
0377 IF (TCZ .LT. TEM1) DPROD=HYD+LIOHL+OML
0378 IF (TCZ .LT. TEM2) DPROD=HYD+LIOHG+OMG
0379 IF (TCZ .GE. TEM1) GO TO 1601
0380 IF (TCZ .GE. TEM2) GO TO 1601
0381 IF (PBMELT .GT. 1338.) DPROD=HYD+LIOHG+OML
0382 IF (PBMELT .LT. 1338.) DPROD=HYD+LIOHL+OMG
0383 QWA=DELH+DPROD-DREAC
0384 IF (IOPTB .EQ. 1) GO TO 22
0385 HTCAPG=CPWOX+CPMNI+CPMLIO+CPA*MA+CPMLIN+CPLIH+MLIH+CPH2*MHZ
      +CPWA+MWA
0386 HTCAPG=HTCAPG/GAMMA
0387 ***** THIS HEAT CAPACITY (CPA) IS GOOD FOR CARBON DIOXIDE ONLY
      CPA=0.175+6.69E-05*TG-1.05E-08*TG**2.
0388 TWO M:LLMETERS ARE ASSUMED TO COVER THE POOL OPTICALLY
0389 ZP=(LILOX/RHOLIO+LILNI/RHOLIN)/ASLI
      IF (EMLI.LT.EMF)EMLI=0.2+(EMF-0.2)*ZP/0.00656
0390 EMG=1.-EXP(-(MLIO/RHOLIO+MLIN/RHOLIN+MLIH/RHOLIH)*2.27E05*CH/V/RA)
0391 EMG=EMG*EMGF
0392 IF (EMG.LT.0.005) EMG=0.005
      THE RIF'S FOR RADIATION FROM THE POOL USE TAUCZ INSTEAD OF (1LIT09830
      FLEXIBILITY
0393 RIFPW=1./(((1.-EMLI)/EMLI+(1.-EMSTL)*ASLI/EMSTL/AW+1./((1.-EMG)
      *(ICZ*(TAUCZ-1.)+1.)+FPW+EMG/(ASLI/AW+1./FPG/(ICZ*(TAUCZ-1.)+1.
      )))
0394 RIFCZW=1./(((1.-EMCZ)/EMCZ+(1.-EMSTL)*ASLI/EMSTL/AW+1./((1.-EMG)
      +EMG/(1.+ASLI/AW)))
0395 RIFPG=EMLI*EMG/(EMG-EMG+EMLI+EMLI/FPG/(ICZ*(TAUCZ-1.)+1.))
0396 RIFCZG=(EMCZ*EMG)/((1.-EMCZ)*EMG+EMCZ)
0397 IF (FLAGS)RIFPAS=1./(((1.-EMINS)/EMINS+(1.-EMSTL)/EMSTL*AINS/AW+
      (AINS/AW+1.)/(1.+AINS/AW*(1.-EMG)))
0398 IF (FLAGS)RIFPAG=EMINS*EMG/(EMINS+EMG-EMINS*EMG)
0399 RIFSLC=(EMSL*EMCONC)/(EMSTL+EMCNC-EMSTL*EMCONC)
0400 RIFCZP=(EMLI*EMCZ)/(EMCZ+EMLI-EMCZ*EMLI),
C ***** CALCULATING GAS HEAT TRANSFER COEFFICIENTS *****
0401 IF (ICZ.EQ.1) T1=0.5*(TG+TCZ)
0402 IF (ICZ.EQ.0) T1=0.5*(TG+TLI)
0403 T2 = 0.5*(TG +TS)
0404 T3E=0.5*(TG+TEHC)
0405 IF (FLAG) T4H=(TS+TA)/2.
0406 IF (.NOT. FLAG) T4H=(TC(NL)+TA)/2.
0407 B1 = 1.0/T1
0408 B2 = 1.0/T2

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0409 B3E=1.0/T3E
0410 B4H=1.0/T4H
0411 D1 = ((4.94E-05*T1 +0.0188)/(RHDA*3600.0))**2
0412 D2 = ((4.94E-05*T2 +0.0188)/(RHDA*3600.0))**2
0413 D3E=(4.94E-05*T3E+0.0188)/(RHDA*3600.0)**2
0414 D4H=(4.94E-05*T4H+0.0188)/(RHDA*3600.0)**2
0415 AK1=(0.014+1.92E-05*(T1-460.))/3600.
0416 AK2=(0.014+1.92E-05*(T2-460.))/3600.
0417 AK3E=(0.014+1.92E-05*(T3E-460.))/3600.
0418 AK4H=(0.014+1.92E-05*(T4H-460.))/3600.
0419 EX2 = (GIN*B2*ABS(TG-TS)/D2)**0.3333
0420 EX3E=(GIN*B3E*ABS(TG-TEHC)/D3E)**0.3333
0421 IF(FLAG)EX4H=(GIN*B4H*ABS(TA-TS)/D4H)**0.3333
0422 IF(.NOT.FLAG)EX4H=(GIN*B4H*ABS(TA-TC(NL))/D4H)**0.3333
0423 H=HING*AK2*EX2
0424 HEHC=HINEHC*AK3E*EX3E
0425 HA=HINSAM*AK4H*EX4H
C*****
C CALCULATING SOME PRELIMINARY THERMAL DIFFUSIVITIES
C BETWEEN NODES (MORE TO COME)
22 B=L(1)/(KCON*2.)*G/KGAP+W/(KSTL*2.)
BB=L(1)/(KCON*2.)*G/KGAP+W/(KSTL*2.)
USUBA=KCON*HA/(KCC*HA*L(NL)/2.)
CT=KSTL*H+W/HICAPG/(W*H/2.*KSTL)*(-1)
C11=KSTL*HA/(RHSTL*CPSTL*W*(KSTL*W*HA/2.))
IF(FLAG) GO TO 779
C3=1./(B*L(1))*RHCON*CPCON
DO 1010 I=1,NLMI
1010 C4(I)=2.*KCON/(RHCON*CPCON*L(I)*(L(I)+L(I+1)))
C5=USUBA/(RHCON*CPCON*L(NL))
C7=1./(B*W)*RHSTL*CPSTL
779 C6=KSTL*H/(RHSTL*CPSTL*W*(W*H/2.*KSTL))
IF (IOPTB .NE. 1) GO TO 878
C1=0.
C6=0.
C8=1./(0.5*W/KSTL/ASLI+0.43/KCON/ASLI)/
.(CPSTL*RHSTL*ASLI*W)
C9=1./(0.5*W/KSTL/ASLI+0.43/KCON/ASLI)/
.(CPCON*RHCON*ASLI*0.86)
878 DO 1020 I=1,NLMI
1020 C10(I)=2.*KCON/(RHCON*CPCON*L(I)*(L(I)+L(I+1)))
IF (IOPTB .EQ. 1) GO TO 524
IF(FLAG) GO TO 780
C8=1./(BB*W)*RHSTL*CPSTL
C9=1./(BB*L(1))*RHCON*CPCON
0443 IF(ICZ.EQ.1) EXX=(GIN*B1*ABS(TCZ-TG)/D1)
0444 IF(ICZ.EQ.0) EXX=(GIN*B1*ABS(TLI-TG)/D1)
0445 IF (EXX .LE. 0.0) GO TO 300
0446 EX1 = (EXX)**0.3333
0447 CEMHC=HEHC*AEHC/HTCAPG
0448 CGSEHC=HEHC*AEHC/XMEHC/CPEHC
0449
0450
0451
0452
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C*****
C CALCULATING GAS CONVECTION COEFFICIENT
DIFF=241.57/(132.0+T1/1.8)*(T1/493.2)**2.5/3600.
0455

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0456 HFINF=HIN*DIFF*EX1
0457 HBINF=HIN*AK1*EX1
0458 IF (TAU -LT. DELT) TAU=DELT
0459 HF=HF+(HBINF-HF)*DELT/TAU
0460 HB=HB+(HBINF-HB)*DELT/TAU
0461 IF (TIME.GT. ESCIN) XESC=1.
0462 IF (TIME.GT. SFLIN) XSFL=1.

0463 C ***** TESTING FOR COMBUSTION *****
0464 ICNI=0
0465 TEZ=(TCZ+TLI)/2.
0466 IF (TEZ.LE.2340. .AND. FOX.LE.0.28 .AND. MNI.GT.0.0) ICNI=1
0467 IF (.NOT.(ILIT.EQ.0 .OR. (ICMB.EQ.0 .AND. ICNI.EQ.0) .OR. TLI -LT.
0468 TMELT)) GO TO 525
0469 IF (ICZ.EQ.1) WRITE(6,529)ICZ,ICNI,ILIT,ICMB,TCZ,FOX,TLI
0470 FORMAT(' COMBUSTION HAS JUST STOPPED. PARAMETERS ARE: ICZ= ',I1,
0471 ' ICNI= ',I1,' ILIT= ',I1,' ICMB= ',I1,' TCZ= ',F8.2,' FOX= ',
0472 ' F7.3,' TLI= ',F8.2)
0473 IF (ICZ.EQ.1) IPAGE=IPAGE+2
0474 GO TO 522
0475 CONTINUE
0476 IF (IOPTB .EQ. 1) GO TO 23
0477 C
0478 C ***** COMPUTATIONS USING COMBUSTION ZONE MODEL *****
0479 C *****
0480 C ***** COMPUTING RATE OF LITHIUM COMBUSTION *****
0481 RN2=0.
0482 ICZ=1
0483 IF (TEZ.LT.1900. .AND. FOX.LE.0.28) RN2=
0484 (1.0-FOX/0.28)/EXP(((1900.-TEZ)/665.)*2.75)
0485 IF (TEZ.GE.1900. .AND. TEZ.LE.2340. .AND. FOX.LE.0.28) RN2=
0486 (1.0-FOX/0.28)*(1.-((TEZ-1900.)/440.)*2)
0487 CMBRO=HF*FOX*RHOA*RCMBO
0488 CMBRN=HF*FNI*RHOA*RCMBN*RN2
0489 CMBRW=HF*FWA*RHOA*RCMBW
0490 CMBR = CMBRN + CMBRN + CMBRW
0491 RNILB=CMBRN*ASLI/RCMBN
0492 ROXLB=CMBRN*ASLI/RCMBO
0493 RNALB=CMBRW*ASLI/RCMBW

0494 C ***** COMPUTATION OF LITHIUM VAPOR DIFFUSION *****
0495 PLIV=(10.** (4.8831-14180.2/TLI))*14.7
0496 RHOLIV=PLIV*144./RIN/TLI
0497 DIFFLI=3.56E-03*((TLI/460.)*+1.-.81)/PA
0498 EFILM=DFILM*12.
0499 C THE FILM THERMAL CONDUCTIVITY IS A WEIGHTED AVERAGE OF NITRO
0500 LITHIUM VAPOR , WITH PLIV AS THE WEIGHTING FACTOR
0501 TFEFF=(TCZ+TLI)/2.+459.67
0502 KNIT=.0432+TFEFF*(.0078-TFEFF*(8.2E-04+TFEFF*2.08E-04))

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0491 KLIT=0.55+TEFF*(-4.99E-04+TEFF*1.206E-07)
0492 KFILM=(PLIV*(KLIT-KNIT)+PA*KNIT)/14.7/3600.

0493 C***** COMPUTATION OF HEAT TRANSFER COEFFICIENTS *****
0494 C THIS HEAT CAPACITY IS SHEER GUESSWORK THE 0.1 IS FOR VERY LOW COMBLIT1190
      YAPCZ=KFILM*AKLI*ASLI/(DFILM*AKLI+KFILM*ZLI/2.)
      CPM CZ=ASLI*((1.+RCMBW)/RCMBD+CMBRO+CPLIO*(1.+RCMBN)/RCMBN+CMBRN*
      . CPLN+((1.+RCMBW)/RCMBW-(1./RCMBH2))-CMBRW*CPWA+(1.+RCMBH2)/
      . RCMH2+CMBRW*CPH2+RN2*HF*FNI*RHOA*CPN2)*300.+1.0
      IF (CPMCZ/ASLI.LE. 0.001) CPM CZ=0.001*ASLI
0495 CGCZ=HB*ASLI/CPMCZ
0496 CCZG=HB*ASLI/HTCAPG
0497 CPCZ=YAPCZ/CPMCZ
0498 CCZP=YAPCZ/(CPLI*LIL)
0500 CCZ=(CMBRO*QCD+CMBRN*QCN+CMBRW*QCW)*ASLI
0501 CLIST=2.*ASLI*AKLI*KSTL/(LIL *CPLI*(ZLI *KSTL+W*AKLI))
0502 CSBLI=2.*AKLI*KSTL/(RHS*TL*W*CPSTL*(ZLI *KSTL+W*AKLI))
0503 IF (IOPTB .EQ. 0) GO TO 852
0504 CMBR=1.
0505 YAPCZ=1.
0506 TG=TLI
0507 RRAD=(3.*RVOL1/4./3.14)**(1./3.)
0508 RAREA=12.57*RRAD**2
0509 LBR=(5.3-RRAD)/2.
0510 LBN=LBR/NA
0511 LB2=LBN/2.
0512 DO 32 J=1,NN
0513 RAD(J)=RRAD*J*LBN
0514 ARE(J)=12.57*RAD(J)**2
0515 VOL(J)=4.19*RAD(J)**3
0516 ATOCZ=RVOL1*2.34
0517 ATICZ=ATOCZ/1.3
0518 QCCZ=1./((5.33/ATOCZ+1.)/(HCO*ATICZ))
0519 AT0(1)=(VOL(1)-RVOL1)*2.34
0520 MB(1)=(VOL(1)-RVOL1)*RHLLI/AMLI
0521 DO 37 J=2,NN
0522 AT0(J)=(VOL(J)-VOL(J-1))*2.34
0523 MB(J)=(VOL(J)-VOL(J-1))*RHLLI/AMLI
0524 DO 24 J=1,NN
0525 ATI(J)=ATO(J)/1.3
0526 A=R1/(2.-J2)
0527 MLI=MLI1-A*MLIOH
0528 MCZ=MCZ1+A*MLIOH+MPB
0529 IF (IG.EQ. 1) CPLIOH=20.74
0530 CPM CZ=MCZ1+CPLZ/MCZ+MPB*CPPZ/MCZ+A*MLIOH+CPLIOH/MCZ
0531 CCZ=(NT+0.025)*((-1.)+QWA-18.*(TCZ-612.))-CPLI*(TCZ-TLI)*R1)/MCZ
0532 IF (ICZ.EQ. 0) CCZ=0.
0533 CF(1)=1./((LB2/(AKLZ+RAREA)+LB2/(AKLI+RAREA))*MCZ*CPMCZ)
0534 CT(1)=1./((LB2/(AKLZ+RAREA)+LB2/(AKLI+RAREA))*MB(1)*CPLI)
0535 DO 33 J=2,NN
0536 CF(J)=(AKLI*ARE(J-1))/LBN/(CPLI*MB(J-1))
0537
0538

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LIT11650
LIT11660

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0539 33 CT(J)=(AKLI*ARE(J-1))/LBN/(CPLI*MB(J))
0540 CLIST=1./((LB2/(AKLI*ARE(NN))+0.5*W/(KSTL*ARE(NN)))+CPLI*MB(NN))
0541 CSBLI=1./((LB2/(AKLI*ARE(NN))+0.5*W/(KSTL*ARE(NN)))+CPLI*MB(NN))
0542 *CPSTL*RHSTL*W*ARE(NN))
0543 TDIF=TCZ-TN(1)
0544 CGZ=0.
0545 CCZG=0.
0546 IF (TDIF .LT. 50.) GO TO 26
0547 IF (TLI .LT. TMELT) GO TO 26
0548 CGCZ=RAREA*AKLI/(RRAD*2.)*(2.0+0.001*((2.65E-04)*(TCZ-TLI)
0549 *RRAD**3)+0.25))/(CPMCZ*MCZ)
0550 CCZG=(RAREA*AKLZ/(RRAD*2.))*(2.0+0.001*((2.65E-04)*(TCZ-TLI)
0551 *RRAD**3)+0.25))/(CPLI*MB(1))
0552 IF (TCZ .GE. 1325.) GO TO 860
0553 GO TO 861
0554 IF (IG .NE. 0) GO TO 862
0555 IG =1
0556 O=CPMCZ*MCZ*ZZ6
0557 MLIO=MLIOH
0558 TIM=MLIOH*OLIOH/Q
0559 MLIT=TIM*NT+0.025
0560 MLIY=MLIT+MLIO
0561 862 IF (MLIOH .LE. MLIY) GO TO 863
0562 861 CGZ=0.
0563 GO TO 852
0564 863 CGZ=1.
0565 IF (IOPTB .EQ. 1) GO TO 2452
0566 ORADP=SICMA*ASLI*(TCZ**4-TLI**4)*RIFCZP
0567 ORADW=SICMA*ASLI*(TCZ**4-TS**4)*RIFCZW
0568 ORADG=SICMA*ASLI*(TCZ**4-TG**4)*RIFCZG
0569 RCZM=ORADW/(W*AW*RHSTL*CPSTL)
0570 RCZP=ORADP/(LIL*CPLI)
0571 RCZG=ORADG/HICAPG
0572 IF (.NOT. FLAG) ORADB=SICMA*ASLI*(TSB**4-TB(1)**4)*RIFSLC
0573 IF (FLAG) ORADB=SICMA*ASLI*(TSB**4-TA**4)*EMSTL
0574 IF (.NOT. FLAG) ORADC=SICMA*AW*(TS**4-TC(1)**4)*RIFSLC
0575 IF (FLAG) ORADC=SICMA*AW*(TS**4-TA**4)*EMSTL
0576 RADG=ORADB/(W*AW*RHSTL*CPSTL)
0577 RADB=ORADB/(W*AW*RHSTL*CPSTL)
0578 IF (.NOT. FLAG) RADCB=ORADB/(LI(1)*ASLI*RHCON*CPCON)
0579 IF (.NOT. FLAG) RADCC=ORADC/(LI(1)*AW*RHCON*CPCON)
0580 ORADY=SICMA*ASLI*(TLI**4-TS**4)*RIFPW
0581 ORADZ=SICMA*ASLI*(TLI**4-TG**4)*RIFPG
0582 RLIY=ORADY/(W*AW*RHSTL*CPSTL)
0583 RLI=ORADY/CPLI/LIL
0584 RGLI=ORADZ/CPLI/LIL
0585 RLI=ORADZ/HICAPG
C*****
C* CALCULATING TEMPERATURE RATES OF CHANGE *
C* (WITH COMBUSTION) *
C*****
IF(IOPTB .EQ. 0) GO TO 1100
0583

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LIT11670  
LIT11680  
LIT11690  
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LIT12140  
LIT12150  
LIT12160  
LIT12170  
LIT12180  
LIT12190



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0584 CONTINUE
0585 Z26=CCZ/CPMCZ-CF(1)*(TCZ-TN(1))-CGCZ*(TCZ-TN(1))
0586 - (QCZ*(TCZ-1032.)-QCZ*180.)/(CPMCZ*MCZ)
0587 ZZ(1)=CT(1)*(TCZ-TN(1))+CGZ*(TCZ-TN(1))-CF(2)*(TN(1)-TN(2))
0588 - (QC(1)*(TN(1)-1032.)-QC(1)*180.)/(CPLI*MB(1))
0589 DO 34 J=2,NO
0590 ZZ(J)=CT(J)*(TN(J)-1)-CF(J+1)*(TN(J)-TN(J+1))
0591 - (QC(J)*(TN(J)-1032.)-QC(J)*180.)/(CPLI*MB(J))
0592 ZZ(NN)=CT(NN)*(TN(NN)-1)-TN(NN)-CLIST*(TN(NN)-TSB)
0593 +CLIST*450.-(OC(NN)*(TN(NN)-1032.)-QC(NN)*180.)/(CPLI*MB(NN))
0594 IF (IOPTB .EQ. 1) GO TO 523
0595 C
0596 CALCULATE COMBUSTION ZONE TEMPERATURE RATE OF CHANGE (DEG. R / SEC.)
0597 1100 Z26=(CCZ-(QRADP+QRADW+QRADG))/CPMCZ-(J-1)*QVAP*CMBR*ASLI/CPMCZ
0598 -CPGZ*(TCZ-TLI)-CGCZ*(TCZ-TG)
0599 IF (TCZ .LT. TLI) Z26=(TLI-TCZ)/DELT
0600 C
0601 CALCULATE LITHIUM TEMPERATURE RATE OF CHANGE (DEG. R / SEC.)
0602 ZZ1=CCZP*(TCZ-TLI)+RCZP-CLIST*(TLI-TSB)+(J-1)*QVAP*CMBR*ASLI*CCZP/
0603 .YAPGZ-RWLI-RGLI+J*CCZG*(TCZ-TLI)
0604 +47800./(CPMLI*MLI)*J
0605 C
0606 CALCULATE CELL GAS TEMPERATURE RATE OF CHANGE (DEG. R / SEC.)
0607 ZZ4=C1*(TG-TS)+CCZG*(TCZ-TG)+RCZG*XBLW+BLWR*CPAB*(TBLOW-TG)
0608 /HTCAPG-ESCR*XESC/HTCAPG+CEHCGS*(TEHC-TG)*RLIG
0609 C
0610 CALCULATE WALL STEEL TEMPERATURE RATE OF CHANGE (DEG. R / SEC.)
0611 IF (.NOT. FLAG) ZZ5=C6*(TG-TS)-C7*(TS-TC(1))+RCZW-RADC*RLIW
0612 IF (FLAG)ZZ5=C6*(TG-TS)-C11*(TS-TA)+RCZW-RADC*RLIW
0613 GO TO 523
0614 C
0615 C*****
0616 C* COMPUTATIONS WITHOUT COMBUSTION ZONE MODEL *
0617 C*****
0618 C
0619 522 CONTINUE
0620 ICZ=0
0621 CMBR=0.0
0622 RN2=0.0
0623 YALIG=AKLI*HB*ASLI/(AKLI+HB*ZLI/2.)
0624 CLIG=YALIG/HTCAPG
0625 QRADW=SIGMA*ASLI*(TLI**4-TS**4)*RIFPW
0626 QRADG=SIGMA*ASLI*(TLI**4-TG**4)*RIFPG
0627 RLW=QRADW/(W*AN*RHSTL*CPSTL)
0628 RWLI=QRADW/CPLI/LIL
0629 RGLI=QRADG/CPLI/LIL
0630 RLIG=QRADG/HTCAPG
0631 IF (.NOT. FLAG1) QRADB=SIGMA*ASLI*(TSB**4-TB(1)**4)*RIFSLC
0632 IF (FLAG1)QRADB=SIGMA*ASLI*(TSB**4-TA**4)*EMSTL
0633 IF (.NOT. FLAG) QRADC=SIGMA*AW*(TS**4-TC(1)**4)*RIFSLC
0634 IF (FLAG)QRADC=SIGMA*AW*(TS**4-TA**4)*EMSTL
0635 RADB=QRADB/(W*ASLI*RHSTL*CPSTL)
0636

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0615 RADC=ORADC/(W*AW*RHSTL*CPSTL)
0616 IF(.NOT. FLAG1) RADC=ORADC/(L1(1)+ASLI*RHCON*CPCON)
0617 IF(.NOT. FLAG) RADC=ORADC/(L1(1)+AW*RHCON*CPCON)
0618 CGLI=VALIG/(LIL*CPIL)
0619 CLIST=2.*ASLI*AKLI*KSTL/(LIL *CPLI*(ZLI *KSTL+W*AKLI))
0620 CSBLI=2.*AKLI*KSTL/(RHSTL*W*CPSTL*(ZLI *KSTL+W*AKLI))
C
C*****
C* CALCULATING TEMPERATURE RATES OF CHANGE *
C* (WITHOUT COMBUSTION) *
C*****
C
CALCULATE LITHIUM TEMPERATURE RATE OF CHANGE (DEG. R / SEC.)
864 ZZI=CGLI*(TG-TLI)-CLIST*(TLI-TSB)-RWLI-RGLI
864 ZZI=CGLI*(TG-TLI)-CLIST*(TLI-TSB)-RWLI-RGLI
C LET COMBUSTION ZONE FOLLOW POOL TEMPERATURE FOR POSSIBLE REIGNITION
ZZ6=(TLI-TGZ)/DELT
C
CALCULATE CELL GAS TEMPERATURE RATE OF CHANGE (DEG. R / SEC.)
ZZA=C1*(TG-TS)+CLIG*(TLI-TG)+RLIG+XBLOW*BLMR+CPAB*(TBLOW-TG)
/HTCAPG-ESCR*XESC/HTCAPG+CEHCGS*(TEHC-TG)
C
CALCULATE WALL STEEL TEMPERATURE RATE OF CHANGE (DEG. R / SEC.)
IF(.NOT. FLAG) ZZ5=C6*(TG-TS)-C11*(TS-TA)+RLIW-RADC
IF(FLAG)ZZ5=C6*(TG-TS)-C11*(TS-TA)+RLIW-RADC
523 CONTINUE
C
C*****
C* COMPUTATIONS VALID WITH EITHER MODEL *
C*****
C
ZZE=CGSEHC*(TG-TEHC)
CALCULATE FLOOR STEEL TEMPERATURE RATE OF CHANGE (DEG. R / SEC.)
IF(.NOT. FLAG)ZZ7=CSBLI*(TLI -TSB)-C8*(TSB-TB(1))-RADC-
XSFL*SFLCR*12./(W*ASLI*RHSTL*CPSTL)
IF(FLAG)ZZ7=CSBLI*(TLI -TSB)-C11*(TSB-TA)-RADB-XSFL*SFLCR*12./
(W*ASLI*RHSTL*CPSTL)
IF(FLAG) GO TO 777
C
CALCULATE WALL CONCRETE TEMPERATURE CHANGE
DTCDT(1)=C3*(TS-TC(1))+C4(1)*(TC(2)-TC(1))+RADC
DTCDT(NL)=C4(NLM1)*(TC(NLM1)-TC(NL))-C5*(TC(NL)-TA)
DO 5 I=2,NLM1
DTCDT(I)=C4(I)*(TC(I+1)-TC(I))+C4(I-1)*(TC(I-1)-TC(I))
777 CONTINUE
C
IF(FLAG) GO TO 778
C
CALCULATE FLOOR CONCRETE TEMPERATURE CHANGE
DTBDT(1)=C9*(TSB-TB(1))+C10(1)*(TB(2)-TB(1))+RADC
DTBDT(NL1)=C10(NLM1)*(TB(NLM1)-TB(NL1))
DO 50 IB=2,NLM1
DTBDT(IB)=C10(IB)*(TB(IB+1)-TB(IB))+C10(IB-1)*(TB(IB-1)-TB(IB))
778 CONTINUE

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IF (ILOPTB .EQ. 1) GO TO 854  
IF (.NOT. FLAGS) GO TO 527

C CALCULATIONS WITH SUSPENDED LITHIUM SPILL PAN  
C

HPAN=0.714+HB  
AHT=ASLI+ZLI\*BREDTH  
TET1=0.0025\*(TINS1-460.)-2.5  
KIN1=(.70892+.36584\*TET1+.04565\*TET1\*\*2-.00791\*TET1\*\*3)/43200.  
TET2=0.0025\*(TINS2-460.)-2.5  
KIN2=(.70892+.36584\*TET2+.04565\*TET2\*\*2-.00791\*TET2\*\*3)/43200.  
YPAGAS=AINS/(THKIN2/2./KIN2+1./HPAN)  
C2=YPAGAS/HTCAPG  
C13=YPAGAS/(RHINS+AINS+THKIN2\*CPINS)  
ORADS=SIGMA\*AINS\*(TINS2\*\*4-TSB\*\*4)\*RIFPAS  
ORADCG=SIGMA\*AINS\*(TINS2\*\*4-TG\*\*4)\*RIFPAG  
RPNST=ORADS/(RHSTL\*AWB+W\*CPSTL)  
RSTPAN=ORADS/(RHINS+AINS+THKIN2\*CPINS)  
RGASPA=ORADCG/(RHINS+AINS+THKIN2\*CPINS)  
RPAGAS=ORADCG/HTCAPG  
CLIPAN=2.\*AHT/(LIL\*CPLI)/(ZLI/AKLI+THKPAN/KPAN)  
CPANLI=2./((RHPAN\*APAN+THKPAN\*CPPAN)/(ZLI/AKLI+THKPAN/KPAN)  
CPNIN1=2./((RHPAN\*APAN+THKPAN\*CPPAN)/(THKPAN/KPAN/APAN+THKIN1/  
KIN1/AINS)  
CIN1PN=2./((RHINS+AINS+THKIN1\*CPINS)/(THKPAN/KPAN/APAN+THKIN1/  
KIN1/AINS)  
CIN12=2./((RHINS\*CPINS+THKIN1)/(THKIN1/KIN1+THKIN2/KIN2)  
CIN21=CIN12\*THKIN1/THKIN2

C ZZ1 =ZZ1 +CLIST\*(TLI -TSB)-CLIPAN\*(TLI -TPAN)  
C ZZ4=ZZ4+C2\*(TINS2-TG)+RPAGAS  
C ZZ7=ZZ7-CSBLI\*(TLI -TSB)+C6\*(TG-TSB)+RPNST

C CALCULATE LITHIUM SPILL PAN TEMP. RATE OF CHANGE (DEG R/SEC)  
C ZZ2=CPANLI\*(TLI -TPAN)+CPNINI\*(TINS1-TPAN)

C CALCULATE INSULATION TEMPERATURE RATE OF CHANGE  
C ZZ8=CIN1PN\*(TPAN-TINS1)+CIN12\*(TINS2-TINS1)  
C ZZ9=CIN21\*(TINS1-TINS2)+C13\*(TG-TINS2)-RSTPAN-RGASPA

C 527 CONTINUE  
C  
C \*\*\*\*\*  
C\*\* CALCULATING OVERPRESSURE \*\*  
C\*\*\*\*\*

XMAIR=MOX/32.+MNI/28.+MA/XMOLA+MMA/18.  
PA=1545.\*XMAIR+TG/144./V  
OVERP=PA-PAZERO

LIT13260  
LIT13270  
LIT13280  
LIT13290  
LIT13300  
LIT13310  
LIT13320  
LIT13330  
LIT13340  
LIT13350  
LIT13360  
LIT13370  
LIT13380  
LIT13390  
LIT13400  
LIT13410  
LIT13420  
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LIT13480  
LIT13490  
LIT13500  
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LIT13680  
LIT13690  
LIT13700  
LIT13710  
LIT13720  
LIT13730  
LIT13740  
LIT13750  
LIT13760  
LIT13770  
LIT13780

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0675 IF (TIME.GT.BLIN) XBLOW=1.
0676 IF (TIME.GT.RLOUT) XBLOW=0.

C *****
C** CALCU. TOTAL LEAKAGE *****
C *****
C AEROSOL REMOVAL COMPUTATION FOR EMG ....
C BETA IS THE INVERSE STICKING COEFFICIENT (IN SECONDS) FOR AEROSOLS
C IMPACTING THE WALL - STICK GIVES THE RATE AT WHICH AEROSOLS
C REMOVED THROUGH STICKING TO THE WALL
C STICK=AW/(V*BETA*12.)
0677

C IF (OVERP)10,10,11
0678 LEAK=0.
0679 GO TO 12
0680 11 LEAK = K*OVERP**0.5
0681 12 CONTINUE
0682 FOUT=EXHSTR/MAIR*XBLOW+LEAK
0683 FMLEFT= EXP(-OUTINT)
0684 FMLEAK = 1. -FMLEFT
0685

C *****
C** DO INTEGRATIONS *****
C *****
C LIBP=INTGRL(O.,CMBR*ASLI)
0686 LILOX=INTGRL(O.,(1.+RCMBO)/RCMBO*CMBRD*ASLI*(1.-FRA))
0687 LIINI=INTGRL(O.,(1.+RCMBN)/RCMBN*CMBRN*ASLI*(1.-FRA))
0688 OXLB=INTGRL(OXLB1,ROXLB)
0689 MOX=INTGRL(MOXI,W02B*BLWR*XBLOW-MOX*FOUT-ROXLB+MOXINJ)
0690 MNI=INTGRL(MNII,WN2B*BLWR*XBLOW-MNI*FOUT-RNILB+MNIINJ)
0691 MA=INTGRL(MAI,WAB*BLWR*XBLOW-MA*FOUT)
0692 MWA=INTGRL(MWAI,WWAB*BLWR*XBLOW-MWA*FOUT)
0693 MLIO=INTGRL(MLIOI,-MLIO*FOUT+(1.+RCMBO)/RCMBO*CMBRD*ASLI*FRA-
0694 MLIO*STICK)
0695 MLIN=INTGRL(MLINI,-MLIN*FOUT+(1.+RCMBN)/RCMBN*CMBRN*ASLI*FRA-
MLIN*STICK)
0696 MLIH=INTGRL(O.,-MLIH*FOUT+((1.+RCMBW)/RCMBW-1./RCMBH2)*CMBRW
*ASLI*FRA-MLIH*STICK)
0697 MH2=INTGRL(O.,-MH2*FOUT+(1.+RCMBH2)/RCMBH2*CMBRW*ASLI)
0698 IF (CGZ.EQ.1.) GO TO 8541
0699 TCZ=INTGRL(TCZI,ZZ6)
0700 GO TO 8542
0701 TCZ=1338.
0702 IOPTB =1
0703 IF (IOPTB.EQ.0) GO TO 855
0704 DO 35 J=1,NN
0705 TN(J)=INTGRL(TLII,ZZ(J))
0706 TLI=TN(4)
0707 TSB=INTGRL(TSZERO,ZZ7)
0708 GO TO 856
0709 TG=INTGRL(TGZERO,ZZ4)
0710 TLI=INTGRL(TLII,ZZ1)

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LII13790

LII13800

LII13810

LII13820

LII13830

LII13840

LII13850

LII13860

LII13870

LII13880

LII13890

LII13900

LII13910

LII13920

LII13930

LII13940

LII13950

LII13960

LII13970

LII13980

LII13990

LII14000

LII14010

LII14020

LII14030

LII14040

LII14050

LII14060

LII14070

LII14080

LII14090

LII14100

LII14110

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LII14130

LII14140

LII14150

LII14160

LII14170

LII14180

LII14190

LII14200

LII14210

LII14220

LII14230

LII14240

LII14250

LII14260

LII14270

LII14280

LII14290

LII14300

LII14310

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0711 IF(TLI.GE.TVAP) GO TO 820
0712 IS=INTGRL(TSZERO,ZZ5)
0713 TPAN=INTGRL(TPANZO,ZZ2)
0714 TINS1=INTGRL(TINS11,ZZ8)
0715 TINS2=INTGRL(TINS21,ZZ9)
0716 TEHC=INTGRL(TEHCZO,ZZE)
0717 DO 750 I=1,NL
0718 TC(I)=INTGRL(TCIC(I),DTCDT(I))
0719
0720 750 CONTINUE
0721 OUTINT=INTGRL(LEAKO,LEAK)
0722 TSB=INTGRL(TSBI,ZZ7)
0723 TB(I)=INTGRL(TBIC(I),DTBDT(I))
0724 CONTINUE
0725 C
C
C CALL DYNAMI (TIME,&200)
C
C*****
C* POST INTEGRATION SECTION
C* CHECK OVERP AND TLI FOR STOP CONDITION
C* CHECK AND CORRECT FOR LITHIUM AND OXYGEN SUPPLY
C*****
C
IF (IOPTB .EQ. 0) GO TO 180
MPB=R2*NT*0.025*TIME
MLIOH=(2.-J2)*NT*0.025*TIME
IF (MLIOH/(2.-J2) .GE. 847.8) ICZ=0
IF (MLIOH/(2.-J2) .GE. 847.8) WRITE(6,879) TIME,MLIOH
FORMAT(1X,'WATER DEPLETED',1X,F6.2,1X,F6.2)
IF (ICZ .EQ. 0 .AND. TCZ .LE. 1340.) GO TO 858
GO TO 503
180 CONTINUE
LILP=LIT-LIBP+LLOX+LILNI
IF (LILP.LE.0.) LILP=0.0
ZLI=LILP/RHLI/ASLI
ALPHA=AKLI/(RHLI*GPLI)
IF ((LILP .LT. 0.1*LIT) .AND. (ALPHA*DELT .GT. ZLI*ZLI .OR. LILP
. .LT. 1.0)) FLAGL=.TRUE.
IF (.NOT. FLAGL) LIL=LILP
IF (TG.LT.500. .AND. OVERP.LT.1.) GO TO 745
IF (TLI .LT. TMELT) GO TO 743
IF (ICMB.EQ.0 .OR. MOX.GE.0.0) GO TO 201
OXLB=OXLFS
ICMB=0
CMBRD=0.0
ROXLB=0.0
201 CONTINUE
IF (LIT.EQ.0 .OR. (LIT-LIBP).GE.0.01) GO TO 500
OXLB=LIT/RCMBO
LILT=0
LIT=LILB
CMBR=0.0
CMBRO=0.0

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- LIT14320
- LIT14330
- LIT14340
- LIT14350
- LIT14360
- LIT14370
- LIT14380
- LIT14390
- LIT14400
- LIT14410
- LIT14420
- LIT14430
- LIT14440
- LIT14450
- LIT14460
- LIT14470
- LIT14480
- LIT14490
- LIT14500
- LIT14510
- LIT14520
- LIT14530
- LIT14540
- LIT14550
- LIT14560
- LIT14570
- LIT14580
- LIT14590
- LIT14600
- LIT14610
- LIT14620
- LIT14630
- LIT14640
- LIT14650
- LIT14660
- LIT14670
- LIT14680
- LIT14690
- LIT14700
- LIT14710
- LIT14720
- LIT14730
- LIT14740
- LIT14750
- LIT14760
- LIT14770
- LIT14780
- LIT14790
- LIT14800
- LIT14810
- LIT14820
- LIT14830
- LIT14840

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0755 CMBRN=0.0
0756 CMBRW=0.0
0757 ROXLB=0.0
0758 RNILB=0.0
0759 RWALB=0.0
0760
0761 500 CONTINUE
0762 IF(MNI.GE.0.0) GO TO 202
0763 MNI=0.0
0764 ICNI=0
0765 CMBRN=0.
0766 RNILB=0.0
0767 202 CONTINUE
0768 IF(MWA.GE.0.0) GO TO 502
0769 MWA=0.0
0770 CMBRW=0.0
0771 RWALB=0.0
0772 502 CONTINUE
0773 CMBRH=3600.*(CMBRO+CMBRN+CMBRW)
0774 IF (CMBRH .GE.0.01 .OR. TIME .LE. 10.) GO TO 503
0775 CMBRO=0.0
0776 CMBRN=0.0
0777 CMBRW=0.0
0778 CMBRH=0.0
0779 ROXLB=0.0
0780 RNILB=0.0
0781 RWALB=0.0
0781 503 CONTINUE
C
C*****
C* CONVERT TEMP. TO DEG. F *
C*****
C
IF (FLAGSI) CALL SI
IF(FLAGSI) GO TO B
DO 6 I=1,20
  TBF(I) =TB(I)-460.
  6 TCF(I)=TC(I)-460.
  YGF=YG-460.
DO 36 I=1,NN
  TNF(I)=TN(I)-460.
  36 TSBF=TSB -460.
  TCF=TCZ-460.
  TLIF=TLI-460.
  TPANF=TPAN-460.
  TEHCF=TEHC-460.
  TINS1F=TINS1-460.
  TINS2F=TINS2-460.
  8 CONTINUE
C
C*****
C* TIME STEP CONTROL *
C*****

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LIT14850
LIT14860
LIT14870
LIT14880
LIT14890
LIT14900
LIT14910
LIT14920
LIT14930
LIT14940
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LIT14960
LIT14970
LIT14980
LIT14990
LIT15000
LIT15010
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LIT15070
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LIT15090
LIT15100
LIT15110
LIT15120
LIT15130
LIT15140
LIT15150
LIT15160
LIT15170
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LIT15250
LIT15260
LIT15270
LIT15280
LIT15290
LIT15300
LIT15310
LIT15320
LIT15330
LIT15340
LIT15350
LIT15360
LIT15370

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0798 IF (IOPTB .EQ. 0) GO TO 865
0799 DT1=ABS(RELERR*TN(1)/ZZ(1))
0800 DT3=ABS(RELERR*TN(4)/ZZ(4))
0801 DT5=1.0E06
0802 IF (ICZ .EQ. 0) GO TO 915
0803 DT5=ABS(RELERR*TCZ/ZZ6)
0804 BILGE=AMINI(DT1,DT3,DT5)
0805 BIL=(BILGE-DELT)/DELT
0806 IF (ABS(BIL) .GT. 0.1) DELT=BILGE
0807 IF (TIME .LT. 8000.) DELOUT=50.
0808 IF (TIME .LT. 20.) DELOUT=1.
0809 IF (TIME .LE. 1.0) DELOUT=0.1
0810 IF (TIME .GE. 8000.) DELOUT=600.
0811 ALPHA1=RHLI*CPMLI/AKLI
0812 ALPHA2=RHSTL*CPSTL/KSTL
0813 ALPHA3=RHCN*CPCON/KCON
0814 T1=0.3*LBN**2/ALPHA1
0815 T2=100.
0816 T3=0.075*W**2/ALPHA2
0817 T4=0.3*0.43**2/ALPHA3
0818 BIT= AMINI(T1,T2,T3,T4)
0819 IF (DELT .GT. BIT) DELT=BIT
0820 IF (DELT.LT.DTMIN) DELT=DTMIN
0821 IF (DELT.GT. DELOUT) DELT=DELOUT
0822 GO TO 866
0823 DT1=ABS(RELERR*TLI/ZZ1)
0824 DT2=ABS(RELERR*TG/ZZ4)
0825 DT3=ABS(RELERR*TS/ZZ5)
0826 IF (ILIT.EQ.0 .OR. ICZ.EQ.0) GO TO 735
0827 DT5=ABS(RELERR*TCZ/ZZ6)
0828 Z299=(CMBRH-CMBRH1)/DELT
0829 DT4=ABS(RELERR*CMBRH/(CMBRH-CMBRH1)*DELT)
0830 CMBRH1=CMBRH
0831 IF (IPASS.EQ.1) DT4=1.E06
0832 GO TO 736
0833 CONTINUE
0834 DT4=1.0E06
0835 DT5=1.0E06
0836 CONTINUE
0837 BILGE=AMINI(DT1,DT2,DT3,DT4,DT5)
0838 BIL=(BILGE-DELT)/DELT
0839 C THIS CONDITION IS TO REMOVE INSTABILITY DUE TO STEEP NITROGEN REACTION
0840 IF (ICZ.GT.1900..AND.ABS(BIL).GT.0.1)DELT=DELT*(BILGE-DELT)/10.
0841 IF (.NOT.(TCZ.GT.1900..AND.ABS(BIL).GT.0.1))DELT=BILGE
0842 IF (TIME .LT. 8000.) DELOUT=50.
0843 IF (TIME .LT. 20.) DELOUT=1.
0844 IF (TIME .LE. 1.0) DELOUT=0.1
0845 IF (TIME .GE. 8000.) DELOUT=600.
0846 TESTING CONDUCTION LIMIT ON TIME STEP ***
0847 ALPHA2=((THKPN+ZLI)/(ZLI/AKLI+THKPN/KPAN))/
    ((RHLI*CPMLI*ZLI+RHPAN*CPPAN+THKPN)/(THKPN*ZLI))
    PYU=0.075*(THKPN+ZLI)**2/ALPHA2

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LIT15380
LIT15390
LIT15400
LIT15410
LIT15420
LIT15430
LIT15440
LIT15450
LIT15460
LIT15470
LIT15480
LIT15490
LIT15500
LIT15510
LIT15520
LIT15530
LIT15540
LIT15550
LIT15560
LIT15570
LIT15580
LIT15590
LIT15600
LIT15610
LIT15620
LIT15630
LIT15640
LIT15650
LIT15660
LIT15670
LIT15680
LIT15690
LIT15700
LIT15710
LIT15720
LIT15730
LIT15740
LIT15750
LIT15760
LIT15770
LIT15780
LIT15790
LIT15800
LIT15810
LIT15820
LIT15830
LIT15840
LIT15850
LIT15860
LIT15870
LIT15880
LIT15890
LIT15900

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0848      PYU=0.075*(THKPAN+ZLI)*2/ALPHA2
0849      IF(DELT.GT.PYU)DELT=PYU
0850      IF(DELT.LT.DTMIN) DELT=DTMIN
0851      IF(DELT.GT.DELOUT) DELT=DELOUT
0852      IF(TIME.LT.1.0) DELT=.10
0853      IF(TCZ.GT.1900. .AND. DELT.GT.20.) DELT=20.
      C
      C*****
      C* OUTPUT SECTION *
      C*****
0866      IF (TIME .LT. TIME0) GO TO 810
0867      TIME=TIME+DELOUT
0868      IF(IPAGE.GE.50) WRITE(6,803) (NAME(I),I=1,92)
0869      803 FORMAT('1',3(20X,20A4.//),32A4)
0870      IF(IPAGE.GE.50) IPAGE=0
0871      IPAGE=IPAGE+1
0872      IF (IOPTB .EQ. 0) GO TO 857
0873      WRITE (6,882) TIME,TCZF,TNF(1),TNF(2),TNF(4),TSBF,TBF(1),MLIOH
0874      FORMAT (7(F9.2,1X),F9.4)
0875      GO TO 810
0876      857 RCCZP=CCZP*(TCZ-TLI)
0877      WRITE (6,804) TIME,DELT,CMBRH,LILP ,OVERP,EMG,EMLI,LIBP,TSF,TGF,
0878      RN2,TCZF,ILIF,TPANF,MOX,MNI
0879      FORMAT(2X,F7.1,1X,4(F6.2,1X),2(F7.2,1X),F8.2,1X,2(F7.2,1X),F6.2,
0880      3(1X,F8.2),2(1X,F9.2))
0881      810 CONTINUE
0882      IF(TIME.GT.TIMEF) GO TO 900
0883      RETURN TO TOP OF DYNAMIC CYCLE
0884      GO TO 200
      C
      C*****
      C* ERROR POINTERS *
      C*****
0885      743 CONTINUE
0886      WRITE(6,744)
0887      744 FORMAT(' POOL TEMP. HAS DROPPED TO LITHIUMS MELTING TEMP. ')
0888      GO TO 900
0889      745 CONTINUE
0890      WRITE(6,746)
0891      746 FORMAT(' CELL GAS TEMP. AND PRESS. HAVE RETURNED TO NORMAL ')
0892      GO TO 900
0893      820 CONTINUE
0894      WRITE(6,821)
0895      821 FORMAT(' LITHIUM TEMP. ABOVE BOILING POINT ')
0896      GO TO 900
0897      910 CONTINUE
0898      WRITE(6,725)
0899      725 FORMAT(1X,' NO ROOT FOUND FOR SPRAY FIRE FOR TEMP.S LESS THAN ',
0900      '1 MILLION DEG. R')
0901      GO TO 900
0902      858 WRITE (6,859) TIME
0903

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LIT15910
LIT15920
LIT15930
LIT15940
LIT15950
LIT15960
LIT15970
LIT15980
LIT15990
LIT16000
LIT16010
LIT16020
LIT16030
LIT16040
LIT16050
LIT16060
LIT16070
LIT16080
LIT16090
LIT16100
LIT16110
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LIT16290
LIT16300
LIT16310
LIT16320
LIT16330
LIT16340
LIT16350
LIT16360
LIT16370
LIT16380
LIT16390
LIT16400
LIT16410
LIT16420
LIT16430

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0007 059  FORMAT ('BREEDER IS COOLING. TIME IS ',F7.1)
0008 GO TO 900
0009 300 CONTINUE
0010 WRITE(6,710)
0011 710 FORMAT(' EXX IS NEGATIVE--CANNOT TAKE ROOT')
0012 WRITE(6,711) TCZ,CMDRH,ZZ6,ZZ5,RN2
0013 711 FORMAT(' MESSED UP VARIABLES',5E10.3)
0014 900 CONTINUE
0015 WRITE(6,713)
0016 713 FORMAT(' PROGRAM EXECUTION STOPPED BY PROGRAM')
0017 WRITE(6,101) DT1,DT2,DT3,DT4,DT5
0018 101 FORMAT(' VALUES', 5E10.3)
0019 C RETURN TO BEGINNING OF PROGRAM AND READ IN NEW DATA. IF NO NEW DATA
0020 C AVAILABLE, PROGRAM EXECUTION WILL AUTOMATICALLY BE STOPPED BY END
0021 C PARAMETER IN THE FIRST STATEMENT.
0022 GO TO 998
0023 999 CONTINUE
0024 CALL EXIT
0025 END
0899
0900
0901
0902
LIT16440
LIT16450
LIT16460
LIT16470
LIT16480
LIT16490
LIT16500
LIT16510
LIT16520
LIT16530
LIT16540
LIT16550
LIT16560
LIT16570
LIT16580
LIT16590
LIT16600
LIT16610
LIT16620

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C THESE 3 SUBROUTINES ARE DESIGNED TO BE USED IN A MAIN PROGRAM WHICH LIT116630
C SIMULATES A DYNAMIC SYSTEM EXPRESSED AS A SET OF ODE'S. THESE ODE'S LIT116640
C MAY BE REEXPRESSED AS A SET OF INTEGRALS WHICH MUST BE INTEGRATED LIT116650
C SIMULTANEOUSLY THROUGH THE DOMAIN OF INTEREST STARTING WITH THE APPLI LIT116660
C INITIAL CONDITIONS. FOR EXAMPLE, THE FUNCTION Y MAY BE FOUND FROM LIT116670
C SOLUTION OF  $dy/dt = \text{RATE} = F(Y, T)$  AND  $y=y_0$  AT  $t=t_0$ . THIS MAY BE LIT116680
C REWRITTEN  $y = \text{INTGRL}(y_0, \text{RATE})$ . THE OPEN INTEGRAL OF RATE OVER T LIT116690
C AT  $y_0$ . A SET OF ODE'S MAY BE TREATED IN A SIMILAR MANNER. LIT116700
C THE MAIN PROGRAM SHOULD CONSIST OF TWO MAIN PARTS, THE INITIAL LIT116710
C SECTION AND THE DYNAMIC SECTION. THE DYNAMIC SECTION IS FURTHER LIT116720
C INTO INTEGRATION AND POST-INTEGRATION SECTIONS. LIT116730
C THE INITIAL SECTION SHOULD BE USED FOR INPUT, CALCULATION OF NELIT116740
C CONSTANTS, AND FOR CALCULATING AND SETTING OF INITIAL CONDITIONS. LIT116750
C SHOULD CONTAIN THE REAL INTGRL, COMMON, AND CALL INIT STATEMENTS. LIT116760
C THE INTEGRATION SECTION SHOULD START WITH A NUMBERED CONTINUE LIT116770
C STATEMENT AND END WITH THE CALL DYNAMI STATEMENT. IT SHOULD CONTALIT116780
C ALL CALCULATIONS OF PROGRAM VARIABLES AND NON-CONSTANT RATES. ALL LIT116790
C FUNCTION STATEMENTS SHOULD APPEAR IN A GROUP IMMEDIATELY PRECEDING LIT116800
C CALL DYNAMI STATEMENT. LIT116810
C THE INTEGRATION SECTION WILL BE LOOPED SEVERAL TIMES DURING EACH LIT116820
C INTEGRATION STEP (SIMPSON'S RULE USES 4 LOOPS PER STEP, RUNGE-KUTTA LIT116830
C 5- LOOPS PER STEP). DYNAMI CONTROLS THE INTEGRATION BY TELLING THE LIT116840
C INTGRL FUNCTION WHAT STEP IT SHOULD PERFORM NEXT. THE INTEGRATION LIT116850
C VARIABLE TIME IS ALSO CONTROLLED BY DYNAMI. IT MAY OR MAY NOT BE LIT116860
C ED DURING EACH LOOP. TIME SHOULD BE INITIALIZED IN THE INTAL SECT LIT116870
C DYNAMI UTILIZES MULTIPLE RETURNS TO CONTROL PROGRAM FLOW. THE STAT LIT116880
C NUMBER PASSED TO DYNAMI SHOULD BE THAT OF THE FIRST STATEMENT IN TH LIT116890
C INTEGRATION SECTION. THIS CAUSES THE PROPER INTEGRATION LOOPING. A LIT116900
C END OF EACH INTEGRATION STEP A NORMAL RETURN IS EXECUTED AND CONTROL LIT116910
C RETURNS TO THE FIRST STATEMENT FOLLOWING CALL DYNAMI. THIS SHOULD B LIT116920
C THE FIRST STATEMENT OF THE POST-INTEGRATION SECTION. LIT116930
C BECAUSE VARIABLE VALUES MAY DIFFER FROM THEIR TRUE VALUE DURING LIT116940
C INTEGRATION LOOPING, ALL PROGRAM LOGIC AND VARIABLE TIME STEP. CAL LIT116950
C EXECUTED ONCE AT THE END OF EACH INTEGRATION STEP. TIME AND ALL VAR LIT116960
C CONTAINED WITHIN THE INTEGRATION SECTION WILL BE UPDATED TO THEIR LIT116970
C VALUES BEFORE CONTROL IS TRANSFERRED TO THE POST-INTEGRATION SECT LIT116980
C THIS SECTION SHOULD CONTAIN AT LEAST ONE IF STATEMENT WHICH STOPS P LIT116990
C EXECUTION. AND THE LAST STATEMENT SHOULD BE A GO TO ST.NO. WHERE SLIT LIT117000
C IS THE STATEMENT NUMBER OF THE FIRST STATEMENT IN THE INTEGRATION SLIT117010
C APPROXIMATELY 100 INTEGRATIONS MAY BE PERFORMED SIMULTANEOUSLY. LIT117020
C LIT117030
C LIT117040
C LIT117050
C LIT117060
C A MATRIX WHICH STORES THE INTERMEDIATE VALUES CALCULATED DURING ELIT117060
C DELT INTEGRATION TIME STEP LIT117070
C DXDT RATE BEING INTEGRATED. CALCULATED USING INTEGRAL VALUE AS LIT117080
C RETURNED BY INTGRL DURING THE PREVIOUS LOOP AND TIME SET BLIT117090
C DYNAMI. USED BY INTGRL AS CALLED FOR BY ICOUNT. LIT117100
C ICOUNT TELLS INTGRL WHICH INTEGRATION LOOP IS PRESENTLY BEING DLIT117110
C IMETH = 1 USE RUNGE-KUTTA METHOD LIT117120
C = 3 USE SIMPSON'S RULE LIT117130
C INDIR TELLS DYNAMI HOW MANY INTGRL STATEMENTS THERE ARE IN THE MLIT117140
C PROGRAM. LIT117150

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C IPASS TELLS INTGRL TO DO TWO SPECIAL FUNCTIONS DURING THE FIRST LIT117160  
 EXECUTIONS OF THE INTEGRATION SECTION.  
 C ISTORE TELLS INTGRL WHERE TO STORE THE RESULT OF ITS INTERMEDIATE LIT117170  
 CALCULATION IN MATRIX A. LIT117180  
 C XIC MATRIX WHICH STORE INITIAL CONDITIONS AND THEN IS UPDATED TLIT17200  
 PRESENT INTEGRAL VALUE AT THE END OF EACH INTEGRATION STEP. LIT17210  
 C XXIC INITIAL CONDITION LIT17220  
 C

0001 SUBROUTINE DYNAMI(TIME,\*)  
 0002 COMMON IMETH,ICOUNT,ISTORE,INDIN,IPASS,DELT,XIC(101),A(501)  
 0003 IF(IPASS.EQ.0) GO TO 40  
 0004 IF(IMETH.EQ.1) GO TO 10

C SIMPSON'S RULE (DEFAULT) IMETH>2  
 C

0005 IF(ICOUNT.EQ.4) GO TO 4  
 0006 IF(ICOUNT.EQ.3) GO TO 3  
 0007 TIME=TIME+DELT/2.  
 0008 ICOUNT=ICOUNT+1  
 0009 RETURN 1  
 0010 CONTINUE  
 0011 ISTORE=0  
 0012 ICOUNT=1  
 0013 IPASS=IPASS+1  
 0014 INDIN=0  
 0015 RETURN

3 CONTINUE  
 ICOUNT =4  
 RETURN 1

C RUNGE-KUTTA METHOD -FIXED STEP- IMETH=1  
 C

0019 10 CONTINUE  
 0020 IF(ICOUNT.EQ.5) GO TO 4  
 0021 IF(ICOUNT.EQ.4) GO TO 14  
 0022 IF(ICOUNT.EQ.2) GO TO 12  
 0023 TIME=TIME+DELT/2.  
 0024 ICOUNT=ICOUNT+1  
 0025 RETURN 1  
 0026 CONTINUE  
 0027 ICOUNT=3  
 0028 RETURN 1  
 0029 CONTINUE  
 0030 ICOUNT= 5  
 0031 RETURN 1  
 0032 CONTINUE  
 0033 IPASS=1  
 0034 RETURN  
 0035 END

C THIS SUBROUTINE INITIALIZES VARIABLES USED BY THE INTEGRATION ROUTINE LIT117650  
 C IT SHOULD BE PLACED IN THE INITIALIZATION SECTION OF THE MAIN PROGRAM LIT117660  
 C BEFORE THE FIRST STATEMENT OF THE DYNAMIC SECTION. SEE DYNAMI FOR LIT117670  
 C LIST AND INTEGRATION DESCRIPTION. LIT117680  
 C LIT117690

0001  
 0002  
 0003  
 0004  
 0005  
 0006  
 0007  
 0008

SUBROUTINE INIT  
 COMMON IMETH,ICOUNT,ISTORE,INDIN,IPASS,DELT,XIC(101),A(501)  
 IPASS=0  
 ISTORE=0  
 ICOUNT=1  
 INDIN=0  
 RETURN  
 END

LIT117700  
 LIT117710  
 LIT117720  
 LIT117730  
 LIT117740  
 LIT117750  
 LIT117760  
 LIT117770

```

0001      REAL FUNCTION INTGRL(XXIC,DXDT)
0002      COMMON IMETH,ICOUNT,ISTORE,INDIN,IPASS,DELT,XIC(101),A(501)
0003      IF(IPASS.EQ.0) GO TO 40
0004      ISTORE=ISTORE+1
0005      IF(IMETH.EQ.1) GO TO 10

0006      C SIMPSON'S RULE (DEFAULT) IMETH GREATER THAN 2
0007      C
0008      C
0009      C
0010      C
0011      C
0012      C
0013      C
0014      C
0015      C
0016      C
0017      C
0018      C
0019      C
0020      C
0021      C
0022      C
0023      C
0024      C
0025      C
0026      C

0027      C
0028      C
0029      C
0030      C
0031      C
0032      C
0033      C
0034      C
0035      C
0036      C
0037      C
0038      C
0039      C
0040      C
0041      C

      FUNCTION INTGRL PERFORMS THE ACTUAL INTEGRATIONS. IN THE MAIN
      PROGRAM, ALL INTGRL STATEMENTS SHOULD BE PLACED IN A GROUP AT THE
      OF THE INTEGRATION SECTION. ALL RATE CALCULATIONS SHOULD PRECEDE
      GROUP AND IT SHOULD BE IMMEDIATELY FOLLOWED BY THE CALL DYNAMI
      FOR VARIABLE LIST AND DESCRIPTIONS SEE DYNAMI.
      REAL FUNCTION INTGRL(XXIC,DXDT)
      COMMON IMETH,ICOUNT,ISTORE,INDIN,IPASS,DELT,XIC(101),A(501)
      IF(IPASS.EQ.0) GO TO 40
      ISTORE=ISTORE+1
      IF(IMETH.EQ.1) GO TO 10

      SIMPSON'S RULE (DEFAULT) IMETH GREATER THAN 2

      IF(ICOUNT.EQ.4) GO TO 4
      IF(ICOUNT.EQ.3) GO TO 3
      IF(ICOUNT.EQ.2) GO TO 2
      1 CONTINUE
      INDIN=INDIN+1
      IF(IPASS.EQ.1) XIC(INDIN)=XXIC
      A(ISTORE)=DXDT
      INTGRL=XIC(INDIN)+DELT*DXDT/2.
      A(500-ISTORE)=INTGRL
      RETURN
      2 CONTINUE
      A(ISTORE)=DXDT
      INTGRL=A(500+INDIN-ISTORE)+DELT*DXDT/2.
      RETURN
      3 CONTINUE
      INTGRL=XIC(ISTORE-2*INDIN)+DELT/6.*(A(ISTORE-2*INDIN)+4.*
      A(ISTORE-INDIN)+DXDT)
      XIC(ISTORE-2*INDIN)=INTGRL
      RETURN
      4 CONTINUE
      INTGRL=XIC(ISTORE-3*INDIN)
      RETURN
      5 CONTINUE
      RUNGE-KUTTA METHOD -FIXED STEP- IMETH=1

      10 CONTINUE
      IF(ICOUNT.EQ.5) GO TO 15
      IF(ICOUNT.EQ.4) GO TO 14
      IF(ICOUNT.EQ.3) GO TO 13
      IF(ICOUNT.EQ.2) GO TO 12
      11 CONTINUE
      INDIN=INDIN+1
      IF(IPASS.EQ.1) XIC(INDIN)=XXIC
      A(ISTORE)=DELT*DXDT
      INTGRL=XIC(INDIN)+.5*A(ISTORE)
      RETURN
      12 CONTINUE
      A(ISTORE)=DELT*DXDT
      INTGRL=XIC(ISTORE-INDIN)+.5*A(ISTORE)
      RETURN

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LIT17780  
LIT17790  
LIT17800  
LIT17810  
LIT17820  
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 LIT18400  
 LIT18410  
 LIT18420  
 LIT18430  
 LIT18440  
 LIT18450  
 LIT18460  
 LIT18470

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0042 13 CONTINUE
0043   A(ISTORE)=DELT*DXDT
0044   INTGRL=XIC(ISTORE-2*INOIN)+A(ISTORE)
0045   RETURN
0046 14 CONTINUE
0047   AA=DELT*DXDT
0048   INTGRL=XIC(ISTORE-3*INOIN)+1./6.*(A(ISTORE-3*INOIN)+2.*
      A(ISTORE-2*INOIN)+2.*A(ISTORE-INOIN)+AA)
      XIC(ISTORE-3*INOIN)=INTGRL
0049   RETURN
0050 15 CONTINUE
0051   INTGRL=XIC(ISTORE-4*INOIN)
0052   RETURN
0053 40 CONTINUE
0054   INTGRL=XXIC
0055   RETURN
0056   END
0057

```

C SI IS USED AT THE OPTION OF THE USER TO CONVERT LITFIRE SO THAT LIT18480  
 C IT ACCEPTS INPUT AND DELIVERS OUTPUT IN SI UNITS  
 C USE JOULES / METERS / SEC / PASCALS  
 C SPECIAL CARE SHOULD BE TAKEN THAT ALL OUTPUT VARIABLES WHICH  
 C MUST BE CONVERTED APPEAR IN THIS SUBROUTINE  
 C

0001 SUBROUTINE SI  
 0002 IMPLICIT REAL (K,L,M)  
 0003 DIMENSION TBF(20),TCF(20),TB(20),TC(20)  
 0004 LOGICAL FLAGJ,FLAGI,FLAGIO  
 0005 COMMON /UNITS/ AW,V,CH,G,KGAP,W,K,HA,HIN,THW,THF,TMELT,TVAP,TCZI,  
 . KPAN,RHPAN,CPAN,TPANZO,APAN,AWB,THKPAN,BREDTH,ASLI,SPILL,QCOI,  
 . QCOZ,QCN,QCM,QVAP,FLAGJ,FLAGI,FLAGIO,BLOW,IESC,ISFLC,RHOLIN,  
 . RHOLIO,RHOLIH,CPA,CPLI,RHLI,AKLI,CPSTL,RHSTL,KSTL,CPCON,RHCON,  
 . KCON,PAZERO,IGZERO,TSZERO,TSBI,TA,TLII,DP1,DP2,DP3,ESCR,SFLCR,  
 . CPAB,IBLOW,EXHSTV,BLOWV,TBF,TCF,THKIN2,THKIN1,AINS,CPINS,RHINS  
 . COMMON /EXTRA/ TINS2F,TB,TC,TG,TGF,TSB,TSBF,TS,TSF,TCZ,  
 . TCZF,TLI,TLIF,TPAN,TPANF,OVERP,MOX,MNI,LILP,HF,HB,EFILM,DFILM,  
 . TINS1,TINS2  
 . IF(FLAGIO) GO TO 1

C INPUT VARIABLES - CHANGE TO ENGLISH  
 C  
 0008 RHOLIO=RHOLIO\*0.06243  
 0009 RHOLIN=RHOLIN\*0.06243  
 0010 RHOLIH=RHOLIH\*0.06243  
 0011 CPA=CPA\*0.000239  
 0012 CPLI=CPLI\*0.000239  
 0013 RHLI=RHLI\*0.06243  
 0014 AKLI=AKLI\*0.5778  
 0015 CPSTL=CPSTL\*0.000239  
 0016 RHSTL=RHSTL\*0.06243  
 0017 KSTL=KSTL\*0.5778  
 0018 CPCON=CPCON\*0.000239  
 0019 RHCON=RHCON\*0.06243  
 0020 KCON=KCON\*0.5778  
 0021 PAZERO=PAZERO\*101325.  
 0022 TGZERO=TGZERO\*1.8  
 0023 TSZERO=TSZERO\*1.8  
 0024 TSBI=TSBI\*1.8  
 0025 TA=TA\*1.8  
 0026 TLII=TLII\*1.8  
 0027 HA=HA\*0.176  
 0028 IF(.NOT. FLAGJ) GO TO 2  
 0029 DP1=DP1\*101325.  
 0030 DP2=DP2\*101325.  
 0031 DP3=DP3\*101325.  
 0032 IF(IESC.EQ.1) ESCR=ESCR\*9.478E-04  
 0033 IF(ISFLC.EQ.1) SFLCR=SFLCR\*9.478E-04  
 0034 IF(1BLOW.EQ.0) GO TO 3  
 0035 CPAB=CPAB\*0.000239  
 0036 TBLW=TBLW\*1.8  
 0037 EXHSTV=EXHSTV\*35.315  
 0038 BLOWV=BLOWV\*2119.  
 2

```

0039      3      AM=AW*10.764
0040      V=V*35.315
0041      CH=CH*3.281
0042      G=G*39.37
0043      KGAP=KGAP*0.5778
0044      W=W*39.37
0045      THW=THW*39.37
0046      THF=THF*39.37
0047      TMELT=TMELT*1.8
0048      TVAP=TVAP*1.8
0049      TCZI=TCZI*1.8
0050      ASLI=ASLI*10.764
0051      SPILL=SPILL*2.205
0052      QCO1=QCO1*0.00043
0053      QCO2=QCO2*0.00043
0054      QCN=QCN*0.00043
0055      QCW=QCW*0.00043
0056      QVAP=QVAP*0.00043
0057      IF(.NOT. FLAGS) GO TO 4
0058      KPAN=KPAN*0.5778
0059      RHPAN=RHPAN*0.06243
0060      CPPAN=CPPAN*0.000239
0061      TPANZO=TPANZO*1.8
0062      APAN=APAN*10.764
0063      AWB=AWB*10.764
0064      THKPAN=THKPAN*39.37
0065      BREDTH=BREDTH*3.281
0066      THKIN1=THKIN1*39.37
0067      THKIN2=THKIN2*39.37
0068      AINS=AINS*10.764
0069      RHINS=RHINS*0.06243
0070      CPINS=CPINS*0.000239
0071      CONTINUE
0072      4
0073      1
0074      C
0075      C
0076      C
0077      C
0078      C
0079      C
0080      C
0081      C
0082      C
0083      C
0084      C
0085      C
0086      C
0087      C
0088      C
0089      C

          OUTPUT VARIABLES - CHANGE TO SI
FLAGID=.TRUE.
DD 7 I=1,20
TBF(I)=TB(I)*0.5556-273.
TCF(I)=TC(I)*0.5556-273.
TGF=IG*0.5556-273.
TSBF=TSB*0.5556-273.
TSF=TS*0.5556-273.
TCZF=ICZ*0.5556-273.
TLIF=LI*0.5556-273.
IF(FLAGS) TPANF=TPAN*0.5556-273.
TINS1F=TINS1*0.5556-273.
TINS2F=TINS2*0.5556-273.
OVERP=OVERP*6893.
MOX=MOX*0.454
MNI=MNI*0.454
LILP=LILP*0.454

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18/07/48

DATE = 80270

SI

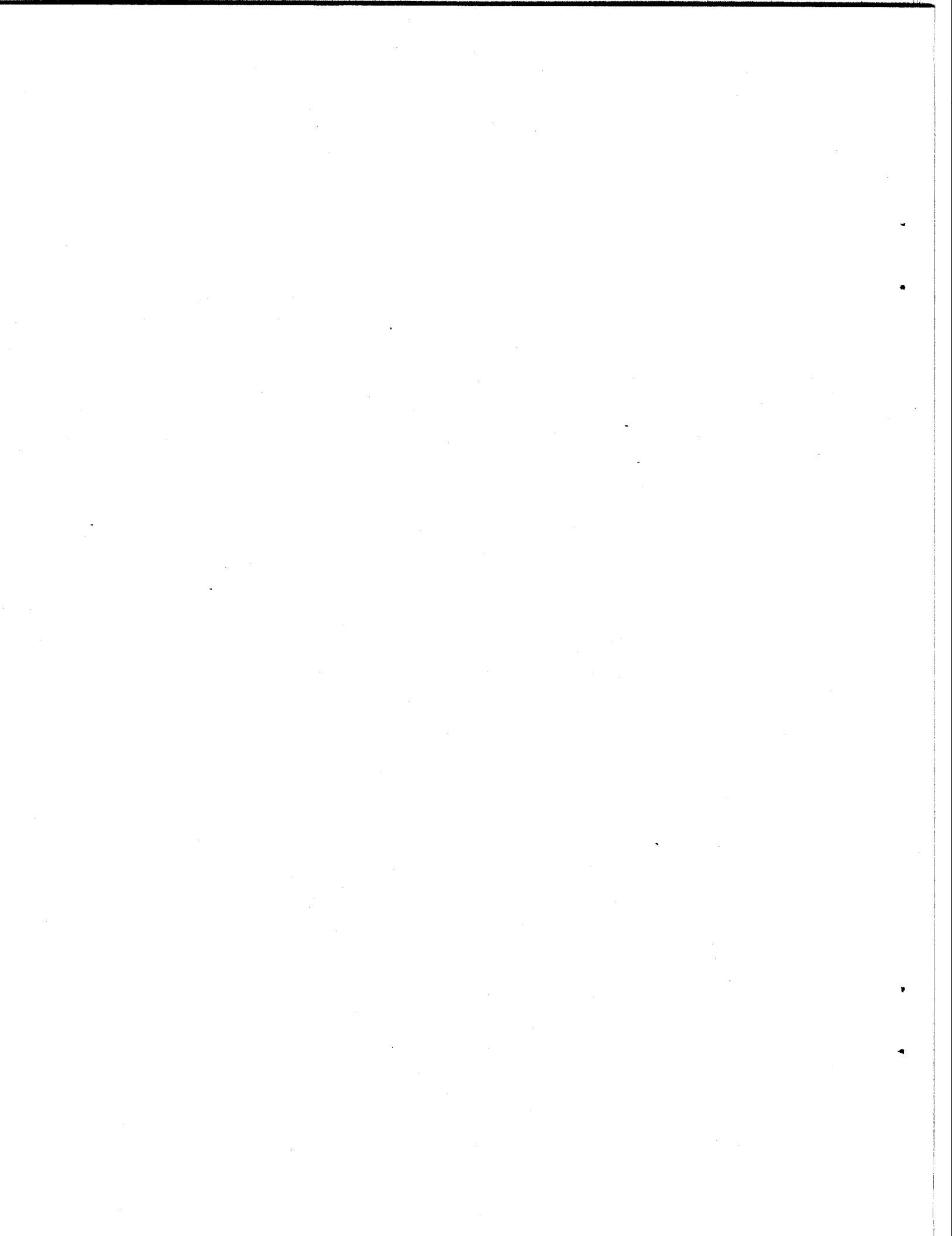
FORTRAN IV G1 RELEASE 2.0

LIT19540  
LIT19550  
LIT19560  
LIT19570  
LIT19580

0090 HF=HF\*0.3048  
0091 HB=HB\*5.68  
0092 EFILM=DFILM\*0.3048  
0093 RETURN  
0094 END

APPENDIX C

Sample Input to LITFIRE



PHYSICAL PROPERTIES

CPLI = 0.0340 RHLI = 617.7000 RHOLIO = 1.0000 AKLI = 20.0200 EMLI = 1.0000  
 CPSTL = 0.1350 RHSTL = 487.0000 RHOLIN = 1.0000 KSTL = 25.0000 EMSTL = 1.0000  
 CPCON = 0.2300 RHCON = 156.0000 RHOLIH = 1.0000 KCON = 15.0000 EMCON = 1.0000  
 KGAP = 1.0000 EMCZ = 1.0000

INNER CONTAINMENT DIMENSIONS

AM = 1.0000 V = 1.0000 THW = 0.0 K = 1.0000  
 CH = 1.0000 W = 0.1260 THF = 41.3000 G = 0.0

SPILL PARAMETERS

ASLI = 354.0000 SPILL = 19700.0000 SPRAY = 0.0 WD2 = 0.0 ZLI = 0.0901  
 FLAGS = F FLAGJ = F FLAGSI = F

HEAT TRANSFER CORRELATION COEFFICIENTS

HIN = 1.0000 HINEHC = 0.0 HINGS = 0.0 HINSAM = 0.0

COMBUSTION PARAMETERS

QCO = 0.0 RCMB0 = 1.0000 TVAP = 4000.0000 RCMBH2 = 1.0000 PERCEN = 0.0  
 QCN = 0.0 RCMBN = 1.0000 TMELT = 915.0000 FRA = 0.0  
 QCW = 6960.0000 RCMBW = 0.3900 QVAP = 1718.0000 RA = 0.0

INITIAL CONDITIONS

TGZERO = 1032.0000 TLLI = 1212.0000 TSBI = 762.0000 WA = 1.0000 PAZERO = 1250.0000  
 TSZERO = 762.0000 TCZI = 1212.0000 TA = 700.0000 WWA = 1.0000

INTEGRATION CONTROL PARAMETERS

IMETH = 3 DTMIN = 0.2000 TIMEF = 6000.0000 RELERR = 0.0060 DELOUT = 2000.0000

OPTIONS IN EFFECT

IBLOW = 0 IESC = 0 ISFLC = 0 FLAG = T FLAG1 = F  
IOPTB = 1

MISCELLANEOUS INPUT

WO2B = 0.0 BLOWV = 0.0 ESCR = 0.0 SFLCR = 0.0 CPA = 1.0000  
WWAB = 0.0 BLOUT = 0.0 ESCIIN = 0.0 SFLTIN = 0.0 CPAB = 1.0000  
WN2B = 0.0 BLIN = 0.0 EXHSTV = 0.0 TBLOW = 1.0000 XMOLA = 1.0000 XMOLAB = 1.0000

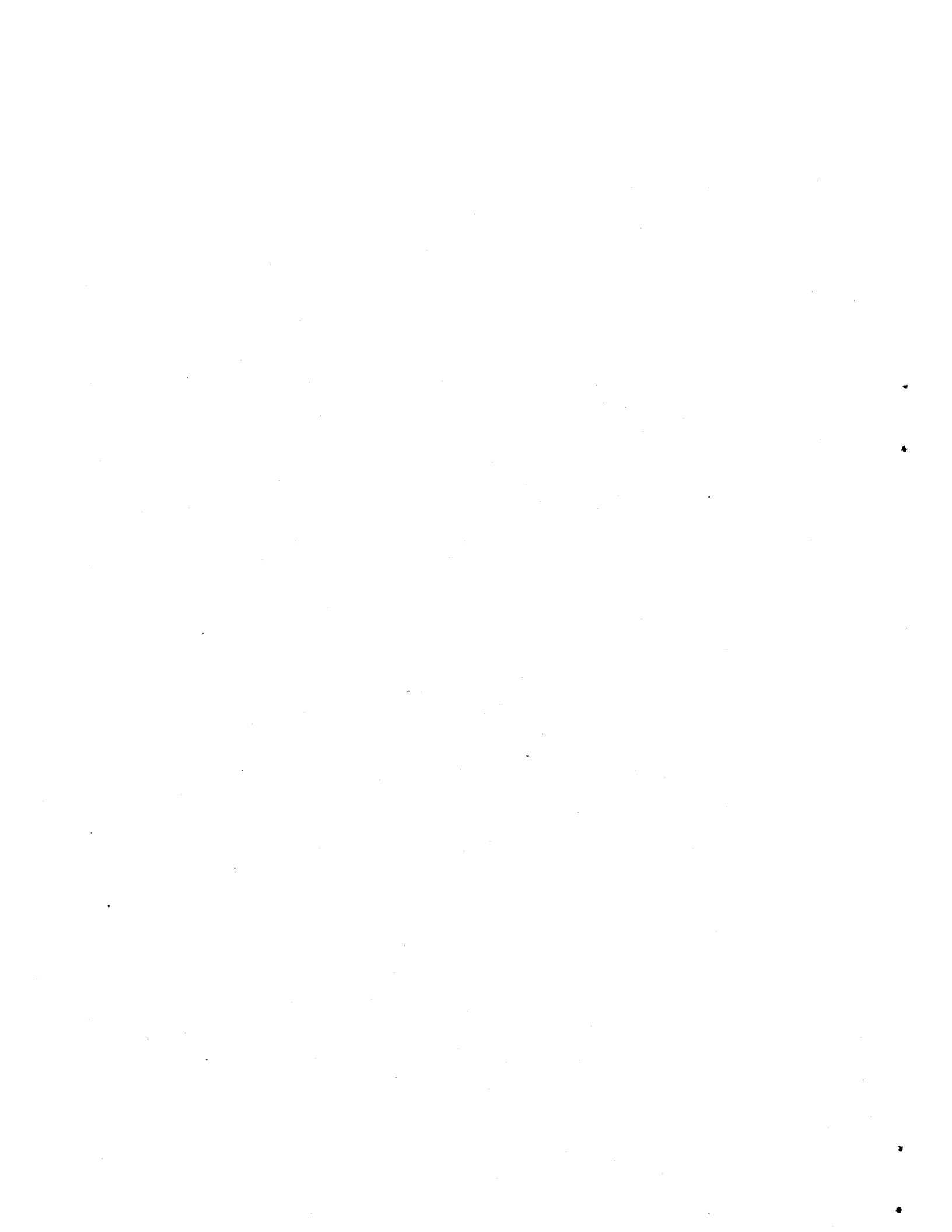
EXTANEIOUS HEAT CAPACITY NODE DATA

TEHCZO = 1300.0000 XMEHC = 0.0 AEHC = 0.0 CPEHC = 1.0000  
INTERNAL BLANKET OPTION INPUT

NT = 3.0 RRAD = 1.00 AMLI = 835.00 HCO = 5.56 QLIOH = 5029.00  
CPLIOH = 12.50 PBMELT = 1081.50 CP1 = 0.028 CP2 = 0.00001 RHPB = 710.00  
AMPB = 207.00 XLI = 0.008 CPPL = 0.033 CPLI1 = 34.35 CPPB1 = 6.93  
R1 = 1.000 R2 = 4.000 J1 = 0.0 J2 = 1.0 QMELT = 2011.70  
QMELTP = 2203.00 DELH = -71560.0

APPENDIX D

Sample Output of LITFIRE



L. 11.4

TIME	T02	T01	T02	T04	T56	T6	MUCH
0.0	752.00	752.00	752.00	752.00	302.00	302.00	0.0
0.10	757.33	752.00	752.00	752.00	304.63	302.00	0.0075
0.20	762.65	752.00	752.00	752.00	307.24	302.00	0.0150
0.30	767.93	752.01	752.00	752.00	309.83	302.00	0.0225
0.40	773.19	752.01	752.00	752.00	312.41	302.00	0.0300
0.50	776.43	752.01	752.00	752.00	314.96	302.00	0.0375
0.60	783.65	752.02	752.00	752.00	317.50	302.00	0.0450
0.70	786.83	752.03	752.00	752.00	320.02	302.00	0.0525
0.80	794.00	752.04	752.00	752.00	322.52	302.00	0.0600
0.90	799.14	752.05	752.00	752.00	325.00	302.00	0.0675
1.00	804.26	752.06	752.00	752.00	327.47	302.00	0.0750
1.10	809.35	752.08	752.00	752.00	329.91	302.00	0.0825
2.10	859.03	752.32	752.00	752.00	353.44	302.02	0.1575
3.10	900.54	753.62	751.82	752.00	373.95	302.03	0.2325
4.10	938.93	754.08	751.83	752.00	394.43	302.06	0.3075
5.10	975.22	754.64	751.84	752.00	413.48	302.09	0.3825
6.10	1009.55	755.29	751.85	752.00	431.22	302.12	0.4575
7.10	1042.04	756.02	751.86	752.00	447.72	302.17	0.5325
8.10	1072.82	756.84	751.87	752.00	463.08	302.21	0.6075
9.10	1102.00	757.73	751.89	752.00	477.38	302.26	0.6825
10.10	1129.66	759.68	751.91	752.00	490.68	302.32	0.7575
11.10	1155.91	759.68	751.92	752.00	503.06	302.38	0.8325
12.10	1180.84	760.75	751.95	752.00	514.58	302.44	0.9075
13.10	1204.51	761.85	751.97	752.00	525.30	302.51	0.9825
14.10	1227.02	763.01	752.00	752.00	535.28	302.58	1.0575
15.10	1248.41	764.20	752.02	752.00	544.57	302.66	1.1325
16.10	1268.77	765.43	752.05	752.00	553.21	302.73	1.2075
17.10	1288.15	766.69	752.09	752.00	561.26	302.81	1.2825
18.10	1306.60	767.98	752.12	752.00	568.74	302.89	1.3575
19.10	1324.18	769.29	752.16	752.00	575.71	302.97	1.4325
20.10	1340.93	770.62	752.20	752.00	582.20	303.06	1.5075
70.29	1672.56	833.53	756.51	752.00	667.63	308.32	5.2721
120.29	1708.40	864.77	761.45	752.03	671.56	313.80	9.0210
170.29	1693.60	876.10	764.68	752.09	673.23	319.20	12.7714
220.28	1666.21	878.83	766.37	752.15	674.79	324.48	16.5211
270.26	1635.69	878.09	767.14	752.21	676.28	329.67	20.2693
320.18	1605.05	876.00	767.43	752.25	677.71	334.76	24.0138
370.11	1575.35	873.41	767.48	752.27	679.09	339.74	27.7583
420.24	1546.87	870.60	767.42	752.28	680.43	344.65	31.5178
470.16	1519.94	867.91	767.30	752.29	681.72	349.45	35.2623
520.29	1494.34	865.21	767.16	752.30	682.97	354.17	39.0218
570.22	1470.23	862.60	767.00	752.30	684.10	358.78	42.7663
620.14	1447.43	860.09	766.83	752.31	685.35	363.31	46.5108
670.27	1425.78	857.66	766.67	752.32	686.49	367.76	50.2702
720.20	1405.36	855.35	766.51	752.33	687.59	372.11	54.0148
770.12	1365.02	853.13	766.35	752.33	688.66	376.38	57.7593
820.25	1367.61	850.99	766.19	752.34	689.71	380.58	61.5188
870.18	1350.22	848.95	766.04	752.35	690.72	384.69	65.2633
920.10	1333.69	847.00	765.89	752.35	691.70	389.73	69.0078
970.23	1317.92	845.12	765.75	752.36	692.67	392.69	72.7672



Li 654

TIME	TC	TL1	F12	TL4	TSB	μE	#COUNT
1020.16	1302.98	843.32	765.61	752.37	693.60	396.57	76.5117
1070.28	1288.69	841.59	765.47	752.37	694.52	400.39	80.2712
1120.21	1275.12	839.93	765.34	752.38	695.41	404.13	84.0157
1170.14	1262.18	838.34	765.21	752.39	696.27	407.80	87.7603
1220.26	1249.78	836.81	765.09	752.39	697.13	411.41	91.5197
1270.19	1237.97	835.34	764.97	752.40	697.95	414.94	95.2642
1320.12	1226.68	833.93	764.84	752.41	698.75	418.41	99.0087
1370.24	1215.83	832.57	764.72	752.41	699.54	421.82	102.7682
1420.17	1205.48	831.26	764.60	752.42	700.31	425.16	106.5127
1470.30	1195.52	829.99	764.48	752.43	701.05	428.46	110.2722
1520.22	1186.00	828.77	764.37	752.44	701.79	431.68	114.0167
1570.15	1176.87	827.61	764.27	752.44	702.51	434.84	117.7612
1620.28	1168.06	826.47	764.18	752.45	703.21	437.96	121.5207
1670.20	1159.63	825.37	764.08	752.46	703.89	441.01	125.2652
1720.13	1151.51	824.33	763.99	752.46	704.56	444.01	129.0097
1770.26	1143.67	823.30	763.90	752.47	705.22	446.96	132.7692
1820.18	1136.16	822.33	763.82	752.48	705.86	449.85	136.5137
1870.11	1128.91	821.37	763.73	752.49	706.48	452.69	140.2582
1920.24	1121.90	820.45	763.65	752.49	707.09	455.50	144.0177
1970.16	1115.16	819.55	763.58	752.50	707.70	458.24	147.7622
2020.29	1108.63	818.69	763.50	752.51	708.29	460.94	151.5217
2070.22	1102.34	817.84	763.42	752.51	708.86	463.59	155.2662
2120.14	1096.27	817.05	763.36	752.52	709.43	466.20	159.0107
2170.27	1090.38	816.25	763.28	752.53	709.98	468.77	162.7702
2220.20	1084.70	815.49	763.22	752.54	710.53	471.28	166.5147
2270.12	1079.20	814.76	763.15	752.55	711.06	473.76	170.2592
2320.25	1073.96	814.02	763.09	752.55	711.58	476.21	174.0187
2370.18	1068.71	813.33	763.02	752.56	712.09	478.60	177.7632
2420.10	1063.71	812.66	762.96	752.57	712.58	480.95	181.5077
2470.23	1058.85	811.98	762.90	752.58	713.07	483.28	185.2672
2520.16	1054.15	811.34	762.84	752.58	713.56	485.55	189.0117
2570.28	1049.57	810.72	762.78	752.59	714.04	487.81	192.7712
2620.21	1045.15	810.11	762.72	752.60	714.50	490.01	196.5157
2670.14	1040.85	809.50	762.66	752.61	714.95	492.18	200.2602
2720.26	1036.65	808.93	762.60	752.62	715.40	494.33	204.0197
2770.19	1032.59	808.38	762.54	752.62	715.83	496.43	207.7642
2820.12	1028.65	807.83	762.49	752.63	716.26	498.50	211.5087
2870.24	1024.80	807.28	762.44	752.64	716.69	500.54	215.2682
2920.17	1021.06	806.76	762.39	752.65	717.11	502.56	219.0127
2970.30	1017.41	806.26	762.35	752.66	717.52	504.53	222.7722
3020.22	1013.87	805.77	762.31	752.67	717.92	506.48	226.5167
3070.15	1010.42	805.28	762.26	752.68	718.31	508.39	230.2612
3120.28	1007.05	804.79	762.22	752.68	718.69	510.29	234.0207
3170.20	1003.78	804.34	762.18	752.69	719.07	512.14	237.7652
3220.13	1000.58	803.90	762.14	752.70	719.44	513.97	241.5097
3270.26	997.46	803.46	762.10	752.71	719.81	515.79	245.2692
3320.18	994.42	803.04	762.07	752.72	720.18	517.56	249.0137
3370.11	991.46	802.61	762.03	752.73	720.54	519.33	252.7582
3420.24	988.56	802.18	761.99	752.74	720.88	521.05	256.5176
3470.16	985.73	801.78	761.96	752.75	721.23	522.76	260.2620

LI PB4

TIME	T(7)	T(13)	T(17)	T(19)	T(21)	T(23)	T(25)	T(27)	T(29)	T(31)	T(33)	T(35)	T(37)	T(39)	T(41)	T(43)	T(45)	T(47)	T(49)	T(51)	T(53)	T(55)	T(57)	T(59)	T(61)	T(63)	T(65)	T(67)	T(69)	T(71)	T(73)	T(75)	T(77)	T(79)	T(81)	T(83)	T(85)	T(87)	T(89)	T(91)	T(93)	T(95)	T(97)	T(99)	T(101)	T(103)	T(105)	T(107)	T(109)	T(111)	T(113)	T(115)	T(117)	T(119)	T(121)	T(123)	T(125)	T(127)	T(129)	T(131)	T(133)	T(135)	T(137)	T(139)	T(141)	T(143)	T(145)	T(147)	T(149)	T(151)	T(153)	T(155)	T(157)	T(159)	T(161)	T(163)	T(165)	T(167)	T(169)	T(171)	T(173)	T(175)	T(177)	T(179)	T(181)	T(183)	T(185)	T(187)	T(189)	T(191)	T(193)	T(195)	T(197)	T(199)	T(201)	T(203)	T(205)	T(207)	T(209)	T(211)	T(213)	T(215)	T(217)	T(219)	T(221)	T(223)	T(225)	T(227)	T(229)	T(231)	T(233)	T(235)	T(237)	T(239)	T(241)	T(243)	T(245)	T(247)	T(249)	T(251)	T(253)	T(255)	T(257)	T(259)	T(261)	T(263)	T(265)	T(267)	T(269)	T(271)	T(273)	T(275)	T(277)	T(279)	T(281)	T(283)	T(285)	T(287)	T(289)	T(291)	T(293)	T(295)	T(297)	T(299)	T(301)	T(303)	T(305)	T(307)	T(309)	T(311)	T(313)	T(315)	T(317)	T(319)	T(321)	T(323)	T(325)	T(327)	T(329)	T(331)	T(333)	T(335)	T(337)	T(339)	T(341)	T(343)	T(345)	T(347)	T(349)	T(351)	T(353)	T(355)	T(357)	T(359)	T(361)	T(363)	T(365)	T(367)	T(369)	T(371)	T(373)	T(375)	T(377)	T(379)	T(381)	T(383)	T(385)	T(387)	T(389)	T(391)	T(393)	T(395)	T(397)	T(399)	T(401)	T(403)	T(405)	T(407)	T(409)	T(411)	T(413)	T(415)	T(417)	T(419)	T(421)	T(423)	T(425)	T(427)	T(429)	T(431)	T(433)	T(435)	T(437)	T(439)	T(441)	T(443)	T(445)	T(447)	T(449)	T(451)	T(453)	T(455)	T(457)	T(459)	T(461)	T(463)	T(465)	T(467)	T(469)	T(471)	T(473)	T(475)	T(477)	T(479)	T(481)	T(483)	T(485)	T(487)	T(489)	T(491)	T(493)	T(495)	T(497)	T(499)	T(501)	T(503)	T(505)	T(507)	T(509)	T(511)	T(513)	T(515)	T(517)	T(519)	T(521)	T(523)	T(525)	T(527)	T(529)	T(531)	T(533)	T(535)	T(537)	T(539)	T(541)	T(543)	T(545)	T(547)	T(549)	T(551)	T(553)	T(555)	T(557)	T(559)	T(561)	T(563)	T(565)	T(567)	T(569)	T(571)	T(573)	T(575)	T(577)	T(579)	T(581)	T(583)	T(585)	T(587)	T(589)	T(591)	T(593)	T(595)	T(597)	T(599)	T(601)	T(603)	T(605)	T(607)	T(609)	T(611)	T(613)	T(615)	T(617)	T(619)	T(621)	T(623)	T(625)	T(627)	T(629)	T(631)	T(633)	T(635)	T(637)	T(639)	T(641)	T(643)	T(645)	T(647)	T(649)	T(651)	T(653)	T(655)	T(657)	T(659)	T(661)	T(663)	T(665)	T(667)	T(669)	T(671)	T(673)	T(675)	T(677)	T(679)	T(681)	T(683)	T(685)	T(687)	T(689)	T(691)	T(693)	T(695)	T(697)	T(699)	T(701)	T(703)	T(705)	T(707)	T(709)	T(711)	T(713)	T(715)	T(717)	T(719)	T(721)	T(723)	T(725)	T(727)	T(729)	T(731)	T(733)	T(735)	T(737)	T(739)	T(741)	T(743)	T(745)	T(747)	T(749)	T(751)	T(753)	T(755)	T(757)	T(759)	T(761)	T(763)	T(765)	T(767)	T(769)	T(771)	T(773)	T(775)	T(777)	T(779)	T(781)	T(783)	T(785)	T(787)	T(789)	T(791)	T(793)	T(795)	T(797)	T(799)	T(801)	T(803)	T(805)	T(807)	T(809)	T(811)	T(813)	T(815)	T(817)	T(819)	T(821)	T(823)	T(825)	T(827)	T(829)	T(831)	T(833)	T(835)	T(837)	T(839)	T(841)	T(843)	T(845)	T(847)	T(849)	T(851)	T(853)	T(855)	T(857)	T(859)	T(861)	T(863)	T(865)	T(867)	T(869)	T(871)	T(873)	T(875)	T(877)	T(879)	T(881)	T(883)	T(885)	T(887)	T(889)	T(891)	T(893)	T(895)	T(897)	T(899)	T(901)	T(903)	T(905)	T(907)	T(909)	T(911)	T(913)	T(915)	T(917)	T(919)	T(921)	T(923)	T(925)	T(927)	T(929)	T(931)	T(933)	T(935)	T(937)	T(939)	T(941)	T(943)	T(945)	T(947)	T(949)	T(951)	T(953)	T(955)	T(957)	T(959)	T(961)	T(963)	T(965)	T(967)	T(969)	T(971)	T(973)	T(975)	T(977)	T(979)	T(981)	T(983)	T(985)	T(987)	T(989)	T(991)	T(993)	T(995)	T(997)	T(999)
3520.29	982.96	801.40	761.93	752.76	721.56	524.44	264.0215																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
3570.22	980.27	801.02	761.90	752.77	721.89	526.09	267.7661																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
3620.14	977.63	800.65	761.86	752.78	722.22	527.74	271.5105																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
3670.27	975.05	800.28	761.83	752.79	722.54	529.34	275.2700																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
3720.20	972.54	799.91	761.80	752.80	722.86	530.93	279.0146																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
3770.12	970.08	799.55	761.77	752.81	723.17	532.51	282.7590																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
3820.25	967.66	799.19	761.74	752.82	723.48	534.04	286.5186																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
3870.18	965.31	798.86	761.71	752.83	723.78	535.57	290.2629																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
3920.10	963.00	798.53	761.69	752.84	724.09	537.08	294.0076																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
3970.23	960.73	798.21	761.66	752.86	724.38	538.55	297.7671																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
4020.16	958.53	797.89	761.64	752.87	724.67	540.02	301.5115																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
4070.28	956.37	797.58	761.61	752.88	724.95	541.49	305.2710																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
4120.26	954.22	797.27	761.59	752.89	725.23	542.91	309.0195																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
4170.26	952.10	796.96	761.56	752.90	725.51	544.35	312.7695																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
4220.26	950.04	796.65	761.53	752.91	725.79	545.79	316.5195																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
4270.26	948.03	796.34	761.50	752.92	726.06	547.18	320.2695																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
4320.26	946.05	796.05	761.48	752.94	726.33	548.55	324.0195																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
4370.26	944.12	795.77	761.46	752.95	726.59	549.93	327.7695																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
4420.26	942.24	795.50	761.44	752.96	726.85	551.29	331.5195																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
4470.26	940.38	795.23	761.42	752.97	727.11	552.61	335.2695																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
4520.26	938.57	794.96	761.40	752.98	727.36	553.92	339.0195																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
4570.26	936.79	794.70	761.38	753.00	727.61	555.23	342.7695																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
4620.26	935.04	794.45	761.36	753.01	727.86	556.52	346.5195																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
4670.26	933.34	794.20	761.34	753.02	728.11	557.77	350.2695																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
4720.26	931.65	793.95	761.32	753.03	728.34	559.02	354.0195																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
4770.26	930.02	793.70	761.30	753.05	728.58	560.27	357.7695																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
4820.26	928.39	793.45	761.28	753.06	728.82	561.51	361.5195																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
4870.26	926.81	793.21	761.26	753.07	729.04	562.70	365.2695																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
4920.26	925.25	792.98	761.24	753.08	729.27	563.88	369.0195																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
4970.26	923.72	792.75	761.23	753.10	729.49	565.07	372.7695																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
5020.26	922.22	792.53	761.21	753.11	729.72	566.26	376.5195																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
5070.26	920.73	792.31	761.20	753.12	729.93	567.41	380.2695																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
5120.26	919.30	792.10	761.18	753.14	730.14	568.53	384.0195																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
5170.26	917.86	791.89	761.17	753.15	730.36	569.66	387.7695																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
5220.26	916.46	791.69	761.16	753.17	730.57	570.78	391.5195																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
5270.26	915.09	791.48	761.14	753.18	730.78	571.91	395.2695																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
5320.26	913.71	791.28	761.13	753.19	730.98	573.00	399.0195																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
5370.26	912.40	791.08	761.12	753.21	731.18	574.06	402.7695																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
5420.26	911.08	790.89	761.10	753.22	731.38	575.12	406.5195																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
5470.26	909.77	790.69	761.09	753.24	731.57	576.18	410.2695																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
5520.26	908.52	790.51	761.08	753.25	731.77	577.25	414.0195																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
5570.26	907.27	790.32	761.07	753.27	731.96	578.31	417.7695																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
5620.26	906.02	790.13	761.05	753.28	732.15	579.32	421.5195																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
5670.26	904.83	789.94	761.04	753.30	732.34	580.32	425.2695																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
5720.26	903.64	789.76	761.03	753.31	732.53	581.32	429.0195																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
5770.26	902.46	789.57	761.02	753.33	732.72	582.32	432.7695																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
5820.26	901.30	789.39	761.00	753.34	732.90	583.32	436.5195																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
5870.26	900.18	789.23	761.00	753.36	733.08	584.32	440.2695																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
5920.26	899.05	789.06	760.99	753.37	733.26	585.28	444.0195																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							
5970.26	897.93	788.89	760.98	753.39	733.43	586.22	447.7695																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																							

LI PB4

TIME	TCZ	TLI1	TLI2	TLI1	TLI2	TLI1	TLI2	TLI1	TLI2	TGB	TGB	MLIoff
6020.26	896.86	788.73	760.97	753.40	733.60	587.16	451.5195					
6070.26	895.79	788.57	760.96	753.42	733.77	588.09	455.2695					
6120.26	894.73	788.41	760.95	753.44	733.94	589.03	459.0195					
6170.26	893.67	788.25	760.94	753.45	734.11	589.97	462.7695					
6220.26	892.66	788.10	760.93	753.47	734.28	590.91	466.5195					
6270.26	891.66	787.95	760.93	753.49	734.44	591.81	470.2695					
6320.26	890.66	787.80	760.92	753.50	734.60	592.69	474.0195					
6370.26	889.66	787.65	760.91	753.52	734.76	593.56	477.7695					
6420.26	888.69	787.50	760.90	753.54	734.92	594.44	481.5195					
6470.26	887.76	787.36	760.90	753.55	735.08	595.31	485.2695					
6520.26	886.82	787.22	760.89	753.57	735.23	596.19	489.0195					
6570.26	885.88	787.08	760.89	753.59	735.39	597.06	492.7695					
6620.26	884.94	786.93	760.88	753.61	735.54	597.94	496.5195					
6670.26	884.05	786.80	760.87	753.62	735.70	598.79	500.2695					
6720.26	883.18	786.67	760.87	753.64	735.84	599.61	504.0195					
6770.26	882.30	786.53	760.86	753.66	735.99	600.42	507.7695					
6820.26	881.43	786.40	760.86	753.68	736.13	601.23	511.5195					
6870.26	880.55	786.27	760.85	753.70	736.28	602.04	515.2695					
6920.26	879.70	786.13	760.85	753.71	736.42	602.86	519.0195					
6970.26	878.89	786.01	760.84	753.73	736.56	603.67	522.7695					
7020.26	878.07	785.88	760.84	753.75	736.70	604.48	526.5195					
7070.26	878.00	785.84	760.84	753.77	736.85	605.29	530.2695					
7120.26	878.00	785.91	760.86	753.79	736.99	606.11	534.0195					
7170.26	878.00	785.99	760.91	753.82	737.12	606.86	537.7695					
7220.26	878.00	786.08	760.96	753.84	737.25	607.61	541.5195					
7270.26	878.00	786.18	761.01	753.86	737.38	608.36	545.2695					
7320.26	878.00	786.27	761.07	753.89	737.51	609.11	549.0195					
7370.26	878.00	786.37	761.12	753.91	737.64	609.86	552.7695					
7420.26	878.00	786.46	761.17	753.93	737.77	610.61	556.5195					
7470.26	878.00	786.56	761.23	753.96	737.90	611.36	560.2695					
7520.26	878.00	786.65	761.28	753.98	738.03	612.11	564.0195					
7570.26	878.00	786.74	761.33	754.01	738.16	612.86	567.7695					
7620.26	878.00	786.84	761.39	754.03	738.29	613.61	571.5195					
7670.26	877.99	786.93	761.44	754.06	738.42	614.35	575.2695					
7720.26	878.00	787.03	761.50	754.08	738.54	615.04	579.0195					
7770.26	878.00	787.12	761.55	754.11	738.67	615.73	582.7695					
7820.26	877.97	787.21	761.60	754.13	738.78	616.42	586.5195					
7870.26	877.83	787.27	761.65	754.16	738.90	617.10	590.2695					
7920.26	877.60	787.32	761.69	754.19	739.02	617.79	594.0195					
7970.26	877.27	787.33	761.72	754.21	739.14	618.48	597.7695					

PROGRAM EXECUTION STOPPED BY PROGRAM  
VALUES 0.845E+04 0.0 0.100E+03 0.0 0.114E+04