

ANALYSIS OF OPERATING"  
DATA RELATED TO POWER  
AND FLOW DISTRIBUTION  
IN A PWR



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MASSACHUSETTS INSTITUTE OF TECHNOLOGY  
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CAMBRIDGE, MASSACHUSETTS

ANALYSIS OF OPERATING DATA RELATED TO  
POWER AND FLOW DISTRIBUTION IN A PWR

by

Henry C. Herbin  
David D. Lanning  
Neil E. Todreas  
Brian W. Kirschner \*  
Alan E. Ladieu \*

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\* Yankee Atomic Electric Co.

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ABSTRACT

The analysis of the effects of the uncertainties associated with temperature and power measurements in the Connecticut Yankee Reactor leads to the evaluation of the uncertainty associated with the effective flow factor. The effective flow factor is defined as the normalized ratio of the average assembly power to the coolant temperature use in each instrumented fuel assembly. Analysis of operating data indicates that the effective flow factor is a measure of the quality of agreement between the reactor physics and the thermal hydraulic analysis of the core. The methods given are also used for the evaluation of the uncertainties associated with the peaking factors, including the results of a sensitivity analysis developed with the code INCORE.

Flow calculations have been performed with the code COBRA III C. The original version of the code COBRA III C has been expanded and a method is given to easily handle any further change in the code. A sensitivity analysis, using the code COBRA III C shows the weak sensitivity of

the exit conditions of the coolant on most input parameters and on the inlet flow distribution of the coolant selected for the calculation. This low sensitivity indicates that the information obtained from the assembly exit thermocouple cannot be used for the determination of the cross flow pattern between the fuel assemblies.

## ACKNOWLEDGMENTS

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CHAPTER 1  
INTRODUCTION

1.1 General Remark

The designer of a reactor is constrained by the requirement that the maximum values of certain design parameters do not exceed critical values. Specific methods are used by the designer such as statistical treatment of hot channel factors, to evaluate the maximum value of a given quantity and the associated confidence level for not exceeding this maximum value.

The reactor operator is provided with different means of control, allowing either a continuous or a discrete monitoring of the critical parameters that can be measured or evaluated from other quantities. The goal is then, to achieve the production of the maximum thermal power, within the limits imposed by the technical specifications. From the reactor operation point of view, it is important to know the actual values of the critical parameters and to see how they compared to the design values. It is also important to include the fact that each parameter can only be evaluated within some uncertainty, since they are either measured or calculated.



The uncertainty in each value comes from the inaccuracy of the control instruments, the inaccuracy due to the calculation method used, and even round off errors due to the use of the computer.

For safety purposes, it is very important to always maintain, an efficient capability for cooling the fuel. The fuel temperatures should be kept as low as possible for a given power level, including the hot spot location. One factor in achieving this requirement is an adequate coolant flow distribution.

This flow distribution depends on specific factors such as: the fuel bundle geometry, the pressure drop distribution, the coolant phase change, the power distribution, etc. Most of the reactor manufacturers orifice the lower core plate, which provides the fuel assembly inlet distribution. The orificing is designed to yield a rather flat temperature distribution of the coolant across the core at the assembly outlet (1).

Unfortunately the flow distribution among the fuel assemblies cannot be measured directly. The problem is even more complex in PWR's than in BWR's, since the PWR fuel assembly is an open geometry assembly type allowing flow and energy exchange between assemblies. In this case the real flow is made up of:

- an axial flow which represents the most important fraction of the total flow,
- a transverse flow or diversion cross flow, representing only a small fraction of the total flow.

As it will be seen later, the flow distribution can be related somewhat to the power distribution. The power distribution among the fuel assemblies is obtained by interpretation of axial neutron flux measurements in instrumented assemblies. This evaluation depends on the accuracy of the flux detectors and the interpretative computation.

## 1.2 Problem Definition

This study has been developed to obtain a better understanding of the effects of the various uncertainties in the control instruments and in the methods of interpretation of the control data in terms of parameters such as peaking factors, power distribution, effective flow factors.

The data used throughout this study came from measurements taken at the Connecticut Yankee Reactor. They have been used to provide actual values of parameters for comparison with the design values of these parameters. Periodically, measurements are made in the Connecticut Yankee Reactor at full power to evaluate and control the time

evolution of:

- the power distribution,
- the location and value of peaking factors:  
 $F_q^N$ ,  $F_z$ ,  $F_{\Delta H}^N$ ,
- the effective flow factors.

The values obtained do not include the effect of the different uncertainties due to the control instruments or the calculation methods and are given in an absolute manner. However, the limits are set to conservatively include these uncertainties.

The problem is to evaluate the effect of these uncertainties on the following quantities:

- local peaking factors,
- effective flow factors,
- power distribution.

Table 1 summarizes the main characteristics of the Connecticut Yankee Reactor.

### 1.3 In-Core Instrumentation of the Connecticut Yankee Reactor

The in-core instrumentation of this reactor is designed to give information on:

- neutron flux distribution using movable neutron flux detectors,

### General characteristics

Thermal power	(MWth)	:	1825
Electrical power	(MWe)	:	617
Reactor manufacturer		:	Westinghouse
Number of loops		:	4

### Core design

Number of fuel assemblies		:	157
Height of the core	(in)	:	126.7
Mass flow for heat transfer	(Mlb/hr)	:	92.7
Fraction of the total flow by-passing the core		:	0.09
Fraction of the total heat generated within the fuel		:	0.974

### Fuel design

Fuel rod OD	(in)	:	0.422
Pellet diameter	(in)	:	0.3835
Active length of fuel	(in)	:	121.8
Fuel array		:	15 x 15
Fuel pitch	(in)	:	0.563
Fuel type		:	UO <sub>2</sub> sintered

Table 1 Summary of the Main Characteristics of the  
Connecticut Yankee Reactor

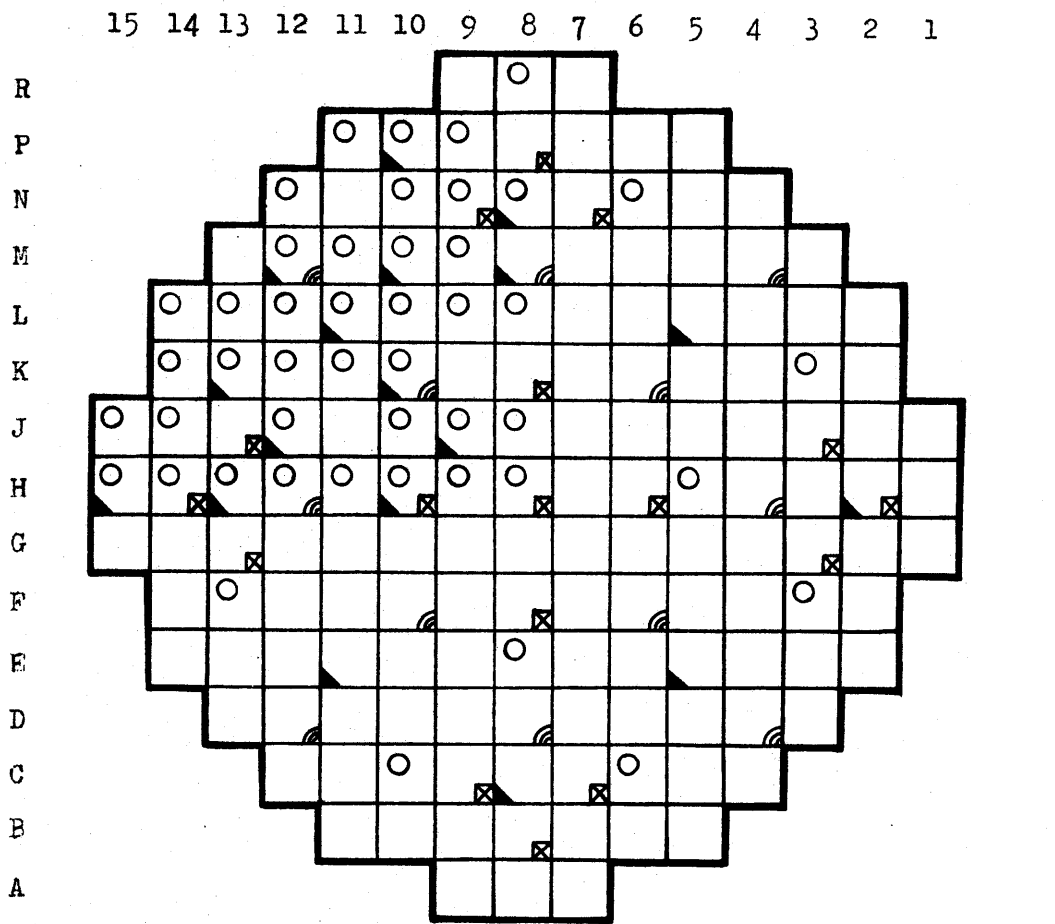
- fuel assembly outlet temperatures using  
Chromel-Alumel thermocouples,

at certain selected locations. Figure 1 shows the in-core instrumentation pattern. One may see that one quadrant of the core is well instrumented, this assumes that the quadrant symmetry holds during the plant life, however, the octant symmetry which exists during the life of the first core, is no longer true after the first refueling.

#### 1.3.1 Thermocouples

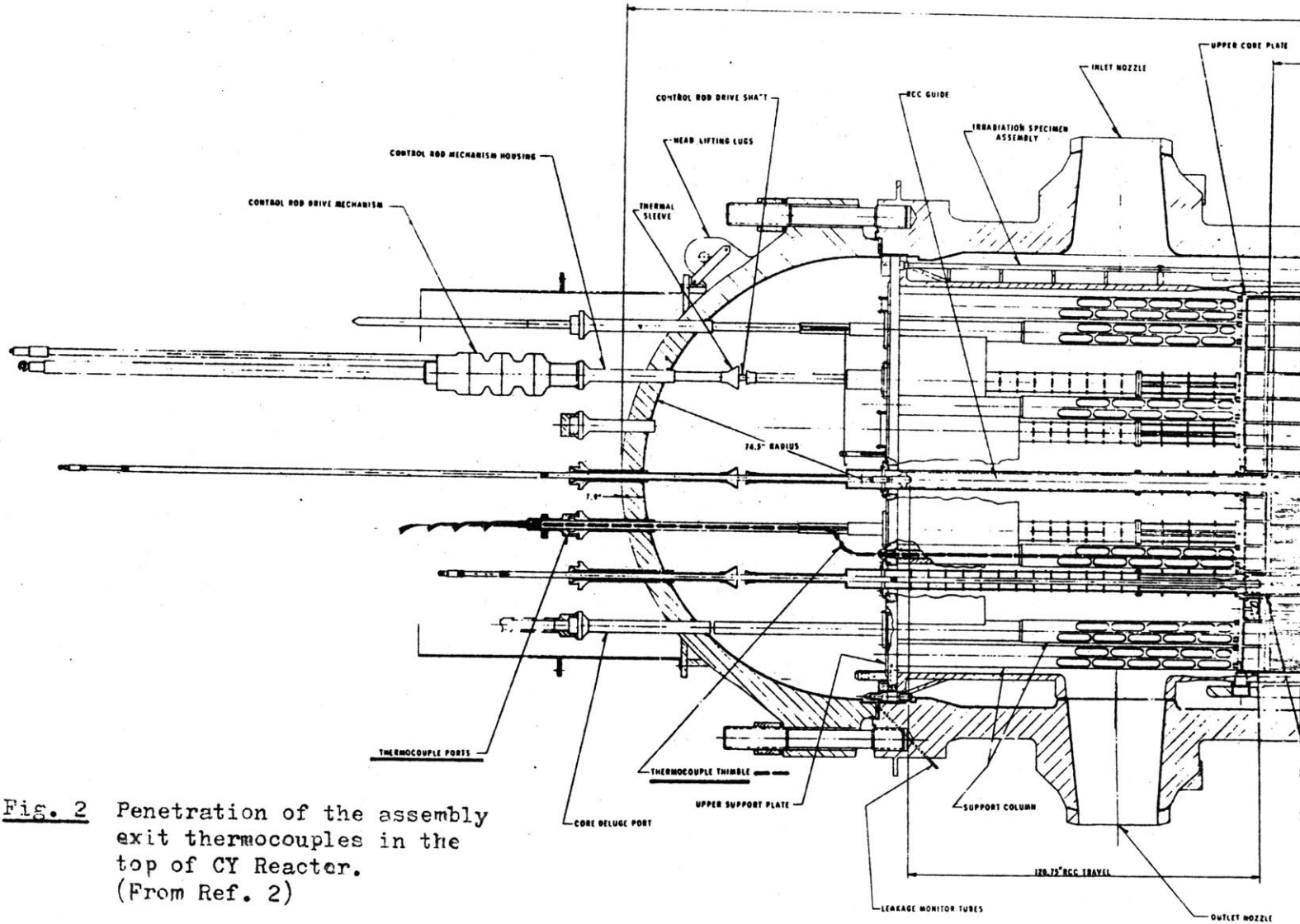
The forty-eight Chromel-Alumel thermocouples penetrate the reactor vessel head through guide-tubes. The guide-tubes are located in some of the support columns which provide adequate rigidity for the upper core plate, whose main function is to hold in position all the fuel assemblies constituting the core.

The thermocouples hot junction are located about 7 inches above the top of the fuel rods and about 13 inches above the top of the heated length. Figures 2 and 3a, b, c, show the thermocouples arrangement in the Connecticut Yankee Reactor. When the coolant leaves the top of the fuel rods it is channeled until it passes the upper core plate and the hot junction of the exit thermocouple. Along this flow path, almost no cross flow ex-



- Key :
- Outlet Thermocouple
  - ▲ In-core flux detector thimble location
  - ⊠ Control rod bank A
  - ▤ Control rod bank B

Fig. 1 In-core instrumentation in the Connecticut Yankee Reactor. (From Ref. 2)



**Fig. 2** Penetration of the assembly  
 exit thermocouples in the  
 top of CY Reactor.  
 (From Ref. 2)

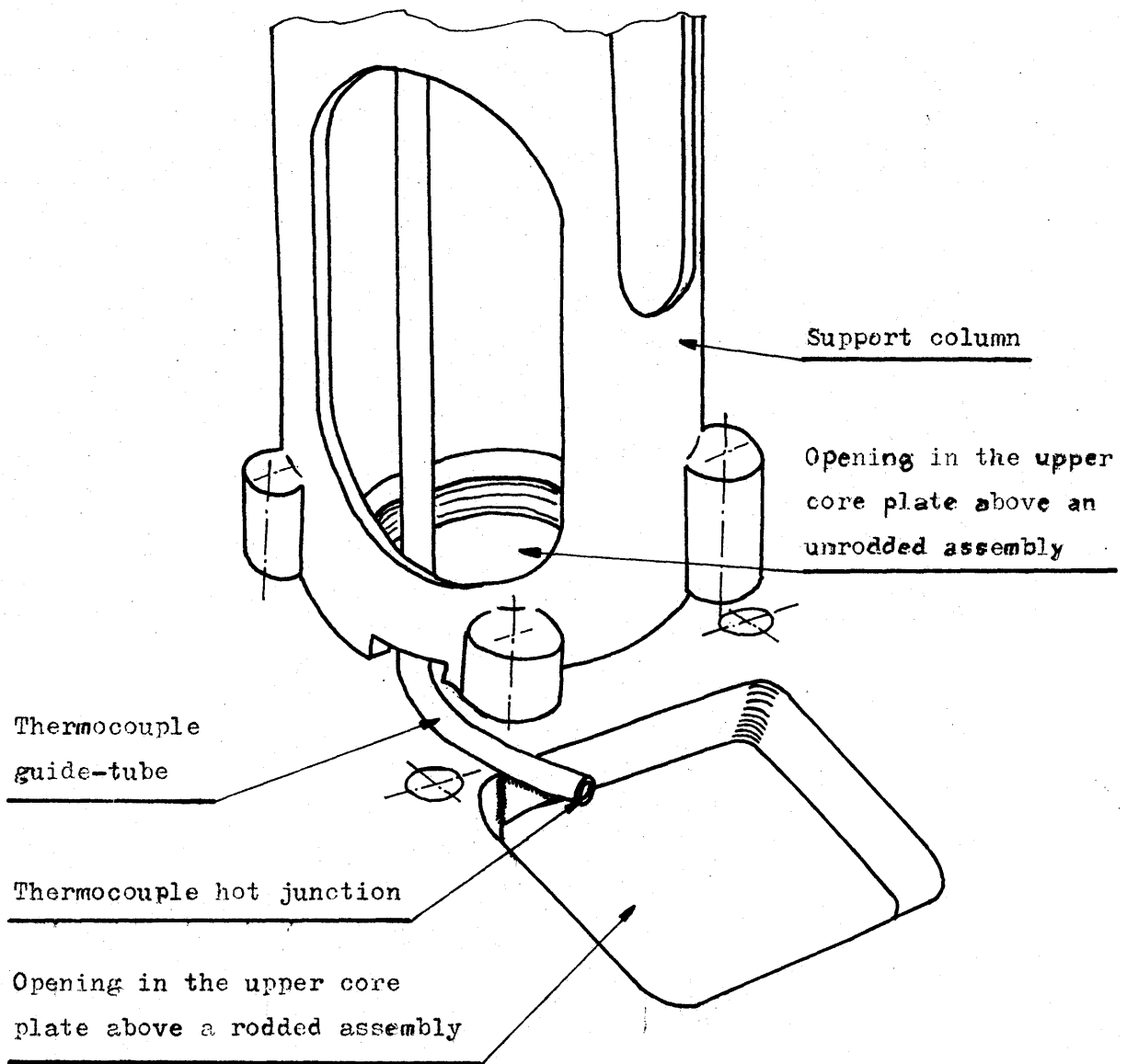


Fig. 3.a Arrangement of the assembly exit thermocouple on the upper core plate. (From Ref. 5)



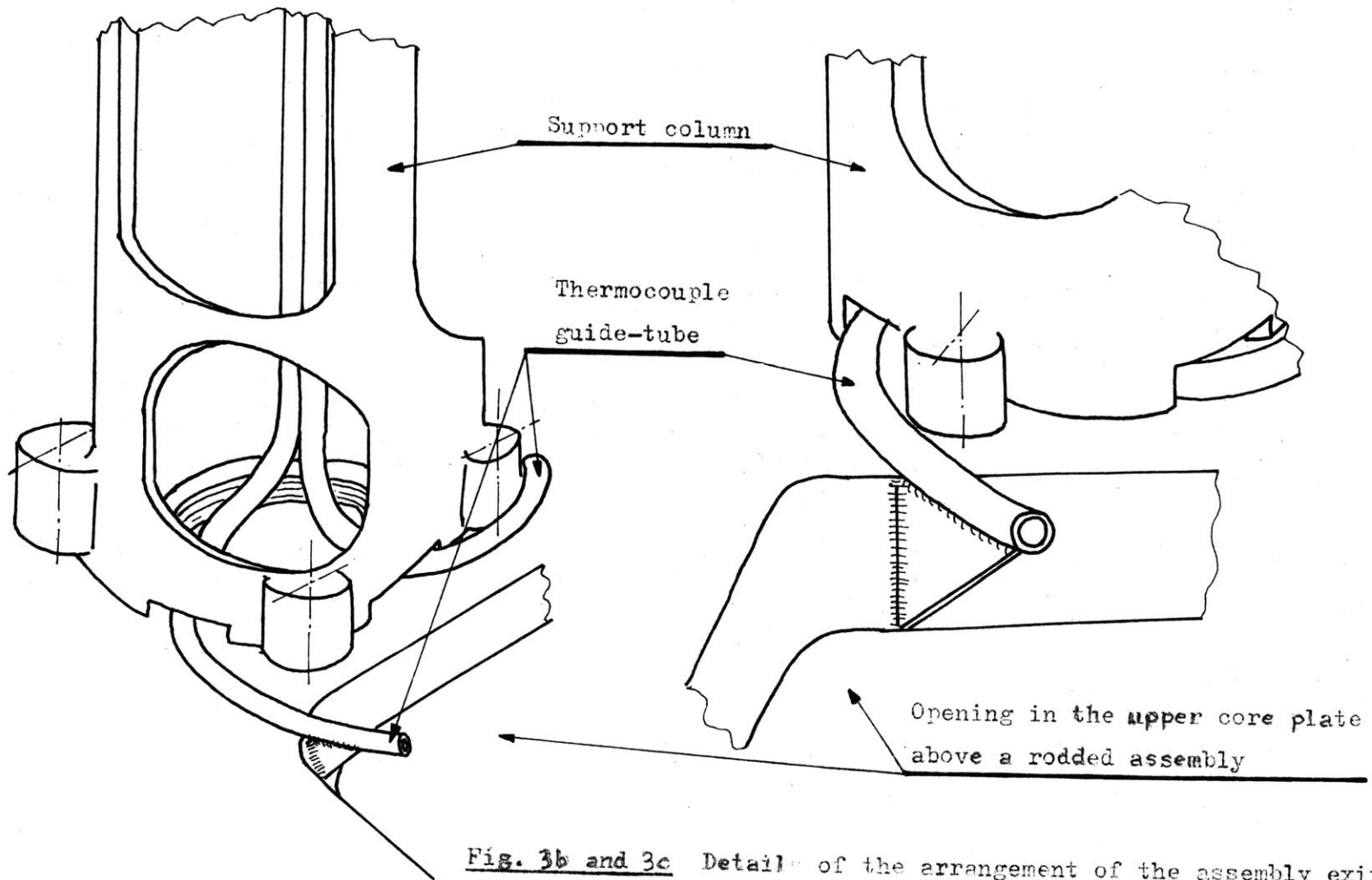


Fig. 3b and 3c Details of the arrangement of the assembly exit thermocouple on the upper core plate.

change with the other fuel assemblies takes place. Therefore the coolant flowing around the hot junction of the exit thermocouple comes only from the top of the fuel rods of the fuel assembly below the thermocouple.

It is interesting to note that in actual operating experience (3) it was not possible to easily replace the defective thermocouples, mainly because they are bent several times in the guide tubes. Design improvements have been made in future reactors so that replacement can be done with less problems.

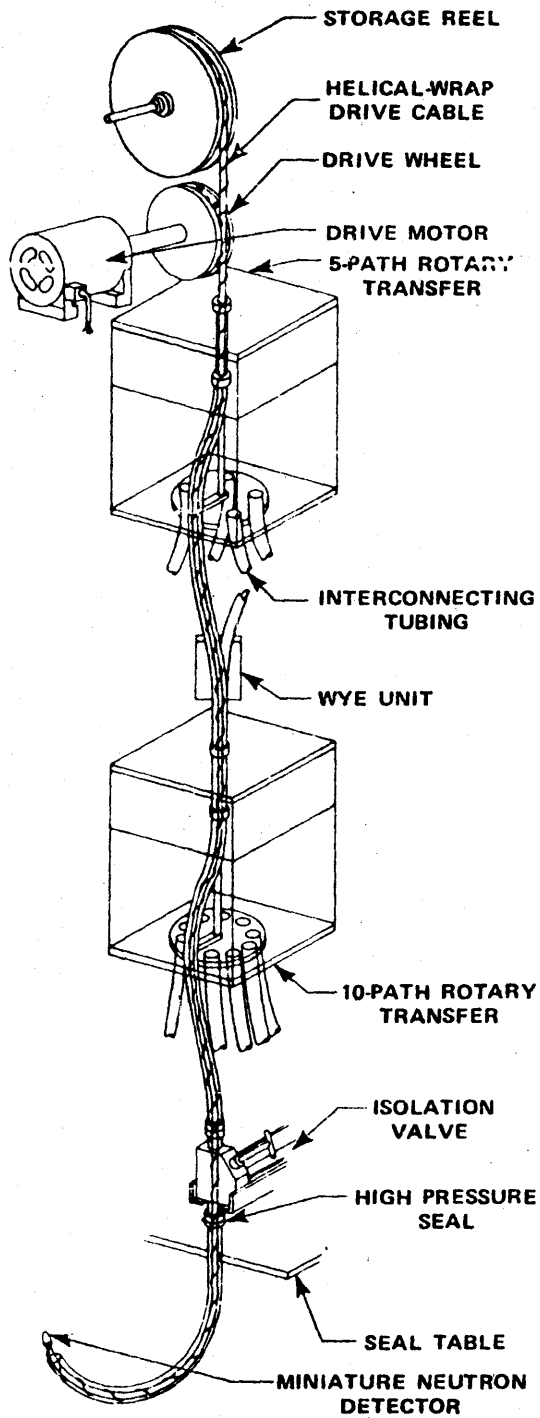
### 1.3.2 Movable Miniature Neutron Flux Detectors

Two fission chamber detectors are used to measure the axial neutron flux. They are made of  $U_3O_8$ , enriched at 90% in  $U^{235}$ . Some of their characteristics are listed below:

Outside diameter:	0.188 in.
Length:	2.0 in.
Minimum neutron sensitivity:	$2 \times 10^{-17}$ amp/nv
Maximum gamma sensitivity:	$3 \times 10^{-14}$ amp/nv
Operating thermal neutron flux range:	$1 \times 10^{11}$ to $4 \times 10^{13}$ nv.

The two fission chambers are under remote control. A complete flux mapping of the core takes about two hours. Each instrumentation thimble in the fuel assemblies is monitored at least once by a flux detector. The neutron flux detector is pushed by a mechanism up to the top of the fuel assembly. Then the detector is pulled, and while it is going from the top to the bottom of the fuel assembly, the neutron flux is recorded. This is done from the top, to be sure of the axial location of the flux detector while the flux is being measured. Otherwise, if the flux were recorded while the flux detector were moving from the bottom to the top of the fuel assembly, there would be a large uncertainty in the detector axial position. Figure 4 represents a typical drive mechanism for in-core movable flux detectors <sup>(4)</sup>. Figure 5 shows a side view of the bottom part of the Connecticut Yankee Reactor <sup>(2)</sup> with the in-core instrumentation system.

During the flux mapping of the core, it happens that the flux can be measured several times at the same location by the two detectors (each enters the same flux thimble at least once). This allows normalization of the two detectors, to account for the fact that they may not have the same cross-section or the same response for a given flux.



**Fig. 4** Typical Drive System for In-Core Instrumentation

(From Ref. 4)

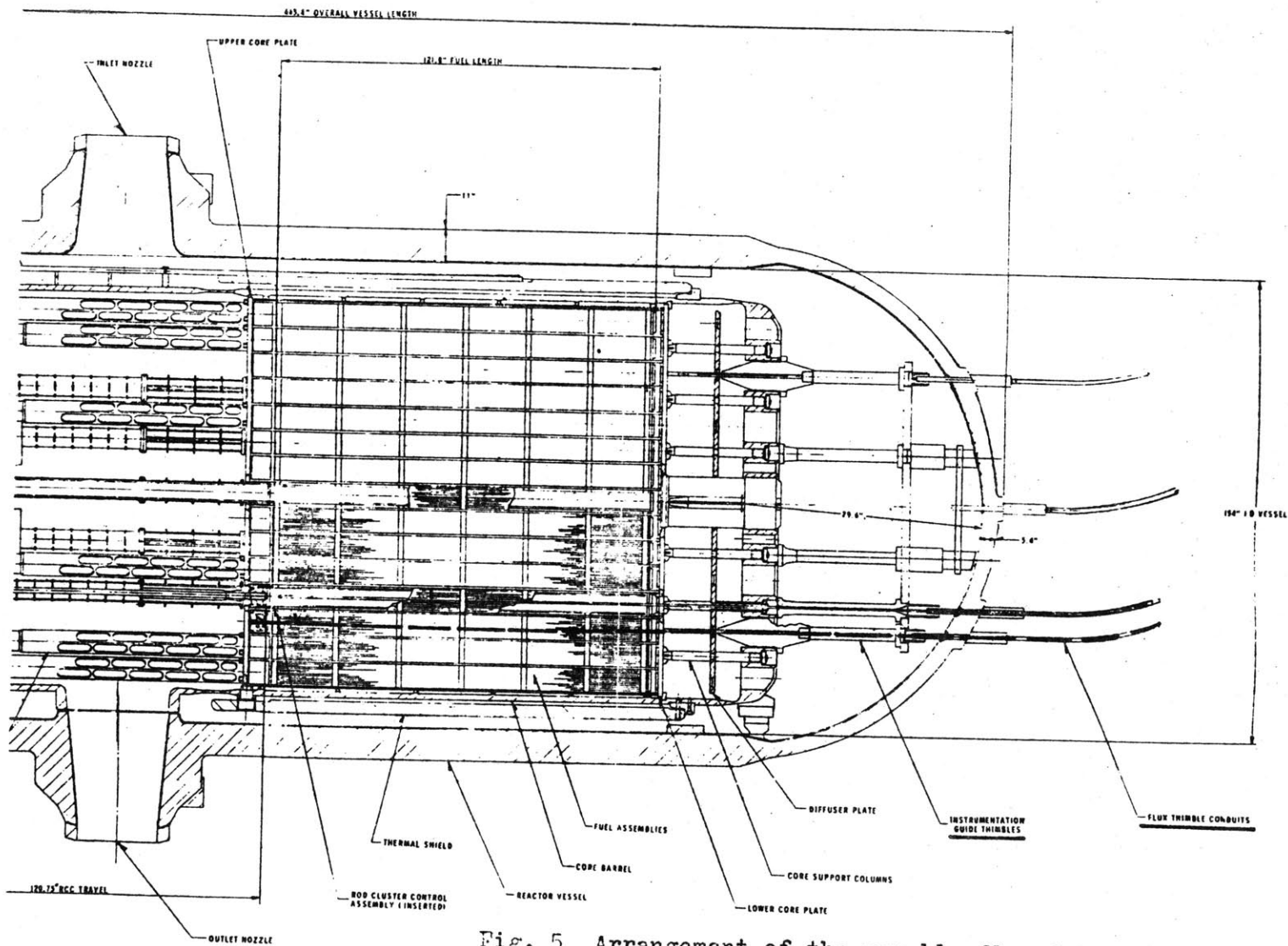


Fig. 5 Arrangement of the movable flux detectors in the bottom of the Connecticut Yankee Reactor. (From Ref. 2)

#### 1.4 Other Instrumentation of the Connecticut Yankee Reactor

##### 1.4.1 Limits of the Description

The description of the rest of the reactor instrumentation used at Connecticut Yankee, will be limited to only the control instruments whose information will be used in this study, i.e. measurement of the reactor pressure, and coolant temperature at the vessel inlet.

##### 1.4.2 Pressure Measurement

The reactor coolant pressure is measured on the hot leg number 4, between the reactor outlet and the stop valve. Two pressure transmitters are used:

- for pressurization and depressurization, a 0 - 1,000 psig pressure transmitter,
- for normal operation, a 0 - 3,000 psig pressure transmitter.

Since the reactor coolant pressure is taken at a location close to the reactor outlet, it may be assumed that this pressure can be taken as the coolant pressure at the core exit.

##### 1.4.3 Inlet Temperature Measurement

The reactor coolant temperature at the vessel inlet is measured by a precision platinum resistance temperature

bulb located on each loop downstream of the steam generator. Other bulbs of this type located upstream and downstream of the steam generator give the loop average temperature and the loop difference temperature.

## CHAPTER 2

### EFFECTIVE FLOW FACTORS

#### 2.1 Definition

It was thought a few years ago, that the time evolution of the "effective flow factor" (defined below) for a given assembly, might give some information on the time history of the coolant flow in this assembly. Further, by considering all the instrumented assemblies in the core, the effective flow factors might also give some indications on the overall core coolant distribution. More precisely, it was expected that a reduction of the value of the effective flow factor in a given assembly, could indicate a change in the channel geometry which caused a partial flow redistribution and a consequent change in the cross flow distribution.

To date only very small variations with time were observed among the effective flow factors, indicating that the channel geometry is unchanged, a fact which has been verified at each refueling.

In the assembly of coordinates  $I, J$ , the effective flow factor  $EFF_{i,j}^*$  can be defined as:

-----  
\* see Nomenclature of the terms used in this study in  
Appendix D.



- the ratio of the relative power  $q_{i,j}$  (assembly power/core average power), to the coolant temperature axial rise  $\Delta t_{i,j}$  in this assembly, over the area of the core limited to the assemblies instrumented with an outlet thermocouple.

where:

$$\Delta t_{i,j} = t_{ou,i,j} - t_{in,i,j}, \quad (2.1)$$

and the effective flow factor  $EFF_{i,j}$  is given by:

$$EFF_{i,j} = \frac{q_{i,j}}{\Delta t_{i,j}} \times \frac{38}{\sum_1 \left( \frac{q_{i,j}}{\Delta t_{i,j}} \right)}, \quad * \quad (2.2)$$

where  $\frac{38}{\sum_1 \left( \frac{q_{i,j}}{\Delta t_{i,j}} \right)}$  represents the normalization factor over

the area of the core limited to the assemblies instrumented with an outlet thermocouple which in the Connecticut Yankee

\* The notation  $\sum_1^{38}$  has the meaning of a sum carried over

the instrumented assemblies in the instrumented quadrant (i.e., 38 assemblies).

case is the area of the core within the instrumented quadrant. This quadrant corresponds to the upper left quadrant on Fig. 1, which shows that 38 assemblies have outlet thermocouples. No credit is taken for the six remaining instrumented assemblies located in the three other quadrants.

## 2.2 Assumption of the Effective Flow Factor

The above effective flow factor definition assumes implicitly the temperature independence of the coolant heat capacity. At a pressure of 2,000 psia a temperature increase of 50°F above an average temperature of 550°F (conditions which are typical of the Connecticut Yankee Reactor), produces a 9% variation of the heat capacity of the coolant.

The temperature dependence of the heat capacity of the water can be taken into account in the computation of the effective flow factors, by replacing the temperature rise  $\Delta t_{i,j}$  by the enthalpy rise  $\Delta h_{i,j}$ , where:

$$\Delta h_{i,j} = h_{ou,i,j} - h_{in,i,j} \quad (2.3)$$

Similar definition of the effective flow factor will lead to:

$$EFF_{1,j} = \frac{q_{1,j}}{\Delta h_{1,j}} \times \frac{38}{\sum_1^{38} \left( \frac{q_{1,j}}{\Delta h_{1,j}} \right)} \quad (2.4)$$

For the same collection of data (relative power distribution and temperature rise distribution), the comparison between the two values of the effective flow factor for a given assembly shows:

- the effective flow factor using the temperature rise is generally not as close to 1.000 as the effective flow factor using the enthalpy rise (a difference of the order of 1% or less).

This comparison is summarized in Fig. 6 for data collected at BOC in Core III. Other comparisons done in Core I and II (not presented here) agree with this observation.

### 2.3 Sensitivity Analysis

Since the effective flow factors are computed from measured and calculated values, it is interesting to determine the contribution of each value used in the calculation of these effective flow factors. In particular the evaluation of the accuracy of the effective flow

	15	14	13	12	11	10	9	8	
R								51.50	1
								0.769	2
								0.8081	3
								0.8110	4
					<u>Hottest assembly- N 11</u>				
P					49.30	53.40	65.90		
					0.737	1.012	1.200		
					0.8086	1.0254	0.9859		
					0.8138	1.0268	0.9721		
N				49.90		56.20	54.10	52.00	
				0.790		0.935	1.016	1.023	
				0.8562		0.9001	1.0160	1.0645	
				0.8611		0.8986	1.0165	1.0677	
M					60.40	61.40	55.50	61.60	
					1.062	1.178	1.158	1.157	
					0.9515	1.0387	1.1297	1.0166	
					0.9447	1.0299	1.1280	1.0077	
L					52.50	62.40	63.90	52.80	53.00
					0.709	1.236	1.182	0.949	0.973
					0.7303	1.0716	1.0008	0.9728	0.9936
					0.7321	1.0612	0.9892	0.9748	0.9953
								54.30	56.40
								0.985	1.088
								0.9817	1.0443
								0.9821	1.0423
K					51.20	53.00	51.10	53.40	52.20
					0.978	0.929	1.163	0.980	1.103
					1.0340	0.9488	1.2321	0.9933	1.1430
					1.0380	0.9505	1.2371	0.9946	1.1461
J					44.10	64.10		61.20	
					0.731	1.238		1.180	
					0.8971	1.0453		1.0434	
					0.9081	1.0329		1.0349	
								58.80	49.90
								1.137	0.926
								1.0460	1.0041
								1.0410	1.0098
H					46.10	50.20	50.30	53.60	58.60
					0.796	0.957	1.199	0.977	1.126
					0.9340	1.0319	1.2905	0.9864	1.0402
					0.9435	1.0373	1.2971	0.9875	1.0355
								48.00	55.20
								0.855	1.032
								0.9639	1.0121
								0.9718	1.0114
									47.00
									0.803
									0.9242
									0.9328

- 1: Measured temperature rise ( $^{\circ}\text{F}$ )
- 2: Relative power of the assembly
- 3: Effective flow factor ( $C_p = \text{constant}$ )
- 4: Effective flow factor ( $C_p = f(T)$ )

Fig. 6 Comparison of the effective flow factor calculation.

factors and the breakdown of this accuracy due to the relative power distribution and temperature rise distribution gives a better understanding of the problems related to the in-core instrumentation.

### 2.3.1 Sensitivity Analysis for Constant Heat Capacity of the Coolant

The effective flow factor is given by Eq. 2.2, which can also be written as:

$$EFF_{i,j} = \frac{q_{i,j}}{\Delta t_{i,j}} \times k, \quad (2.5)$$

where:

$$k = \frac{38}{\sum_1 \left( \frac{q_{i,j}}{\Delta t_{i,j}} \right)} \quad (2.6)$$

If we define:

$\sigma_{rq_{i,j}}$  = relative standard deviation of the relative power,

$\sigma_{t_{ou,i,j}}$  = standard deviation of the assembly outlet temperature,

$\sigma_{t_{in,i,j}}$  = standard deviation of the assembly inlet temperature.

The square of the relative standard deviation of the effective flow factor is given by:

$$\sigma_r^2 \text{EFF}_{i,j} = \frac{\sum_1^{38} \sigma^2 \left( \frac{q_{i,j}}{\Delta t_{i,j}} \right)}{\left[ \sum_1^{38} \left( \frac{q_{i,j}}{\Delta t_{i,j}} \right) \right]^2} + \sigma_r^2 q_{i,j} + \frac{\sigma^2 t_{ou,i,j}}{\Delta t_{i,j}^2} + \frac{\sigma^2 t_{in,i,j}}{\Delta t_{i,j}^2} \quad * \quad (2.7)$$

The square of the standard deviation of the effective flow factor is given by:

$$\sigma^2 \text{EFF}_{i,j} = \left[ \frac{q_{i,j}}{\Delta t_{i,j}} \right]^2 \times \frac{k^2}{\left[ \sum_1^{38} \left( \frac{q_{i,j}}{\Delta t_{i,j}} \right) \right]^2} \quad (2.8)$$

---

\* See Appendix E for the derivation of Eqs. 2.7, 2.8, and 2.9.

$$\begin{aligned}
& \times \sum_1^{38} \sigma^2 \left( \frac{q_{1,j}}{\Delta t_{1,j}} \right) \left. \begin{array}{l} \text{component due to the} \\ \text{normalization} \end{array} \right\} \\
& + \left[ \frac{k}{\Delta t_{1,j}} \right]^2 (\sigma_r^2 q_{1,j}) \frac{q_{1,j}^2}{\Delta t_{1,j}} \left. \begin{array}{l} \text{component due to the} \\ \text{power distribution} \end{array} \right\} \\
& + \left[ \frac{k q_{1,j}}{\Delta t_{1,j}^2} \right]^2 \sigma^2 t_{ou,i,j} \left. \begin{array}{l} \text{component due to the} \\ \text{outlet temperature} \end{array} \right\} \\
& + \left[ \frac{k q_{1,j}}{\Delta t_{1,j}^2} \right]^2 \sigma^2 t_{in,i,j} \left. \begin{array}{l} \text{component due to the} \\ \text{inlet temperature} \end{array} \right\}
\end{aligned}$$

(2.8)  
(continued)

But the component due to the normalization can be split into:

$$\left[ \frac{q_{1,j}}{\Delta t_{1,j}} \right]^2 \times \frac{k^2}{\left[ \sum_1^{38} \left( \frac{q_{1,j}}{\Delta t_{1,j}} \right) \right]^2} \times \sum_1^{38} \sigma^2 \left( \frac{q_{1,j}}{\Delta t_{1,j}} \right) = \quad (2.9)$$

$$\left[ \frac{q_{i,j}}{\Delta t_{i,j}} \right]^2 \times \frac{k^2}{\left[ \sum_1^{38} \left( \frac{q_{i,j}}{\Delta t_{i,j}} \right) \right]^2} \times \sum_1^{38} \left( \frac{q_{i,j}}{\Delta t_{i,j}} \right)^2$$

$$\left[ \begin{array}{l} \sigma_r^2 q_{i,j} \\ + \frac{\sigma_{t_{ou,i,j}}^2}{\Delta t_{i,j}^2} \\ + \frac{\sigma_{t_{in,i,j}}^2}{\Delta t_{i,j}^2} \end{array} \right] \left\{ \begin{array}{l} \text{term due to the power} \\ \text{term due to the outlet} \\ \text{temperature} \\ \text{term due to the inlet} \\ \text{temperature.} \end{array} \right.$$

(2.9)  
(continued)

The total contribution of the power distribution, the outlet and inlet temperatures is the sum of the corresponding terms in Eqs. 2.8 and 2.9.

A code called FLOFA I has been written to calculate the standard deviation on the effective flow factor (see Appendix B for the code listing and sample input and



output). From the data, relative power and temperatures distributions, the code is used to compute:

- the effective flow factor distribution,
- the standard deviation of the effective flow factor,
- the breakdown of the square of the standard deviation of the effective flow factor into components due to:
  - normalization,
  - power distribution,
  - outlet temperature,
  - inlet temperature.

This is done for assumed values of standard deviation on relative power distribution and inlet and outlet temperatures. These values can be varied by the user.

### 2.3.2 Sensitivity Analysis for Temperature Dependent Heat Capacity of the Coolant

Similar work has been done in this section as in 2.3.1. By using Eq. 2.4 to define the effective flow factor:

$$EFF_{1,j} = \frac{q_{1,j}}{\Delta h_{1,j}} \times \frac{38}{\sum_1 \left( \frac{q_{1,j}}{\Delta h_{1,j}} \right)} = \frac{q_{1,j}}{\Delta h_{1,j}} \times k_t \quad , \quad (2.10)$$

where:

$$k_t = \frac{38}{\sum_1^{38} \left( \frac{q_{i,j}}{\Delta h_{i,j}} \right)}$$

The square of the relative standard deviation of the effective flow factor is given by:

$$\sigma_r^2 \text{ EFF}_{1,j} = \frac{\sum_1^{38} \sigma^2 \left( \frac{q_{i,j}}{\Delta h_{i,j}} \right)}{\left[ \sum_1^{38} \left( \frac{q_{i,j}}{\Delta h_{i,j}} \right) \right]^2} + \sigma_r^2 q_{i,j} + \frac{\sigma^2 h_{ou,i,j}}{\Delta h_{i,j}^2} + \frac{\sigma^2 h_{in,i,j}}{\Delta h_{i,j}^2} \quad * \quad (2.11)$$

---

\* See Appendix E for derivation of Eqs. 2.11, 2.12, and 2.13.

The square of the standard deviation of the effective flow factor is given by:

$$\begin{aligned}
 \sigma^2_{EFF_{i,j}} = & \left[ \frac{q_{i,j}}{h_{i,j}} \right]^2 \times \frac{k_t^2}{\sum_1^{38} \left( \frac{q_{i,j}}{\Delta h_{i,j}} \right)} \times \sum_1^{38} \sigma^2 \left( \frac{q_{i,j}}{\Delta h_{i,j}} \right) \\
 & \left. \begin{array}{l} \text{component due to the} \\ \text{normalization} \end{array} \right\} \\
 + & \left[ \frac{k_t}{\Delta h_{i,j}} \right]^2 \left[ \sigma_r^2 q_{i,j} \right] q_{i,j}^2 \left. \begin{array}{l} \text{component due to} \\ \text{the power} \end{array} \right\} \\
 + & \left[ \frac{k_t q_{i,j}}{\Delta h_{i,j}^2} \right]^2 \left[ \frac{\partial h_{ou,i,j}}{\partial t_{ou,i,j}} \right]^2 \sigma^2_{t_{ou,i,j}} \left. \begin{array}{l} \text{component due} \\ \text{to the outlet} \\ \text{temperature} \end{array} \right\} \\
 + & \left[ \frac{k_t q_{i,j}}{\Delta h_{i,j}^2} \right]^2 \left[ \frac{\partial h_{in,i,j}}{\partial t_{in,i,j}} \right]^2 \sigma^2_{t_{in,i,j}} \left. \begin{array}{l} \text{component due} \\ \text{to the inlet} \\ \text{temperature} \end{array} \right\}
 \end{aligned}$$

(2.12)

Splitting the component due to the normalization  
would lead to:

$$\left[ \frac{q_{i,j}}{\Delta h_{i,j}} \right]^2 \times \frac{k_t^2}{\left[ \sum_1^{38} \left( \frac{q_{i,j}}{\Delta h_{i,j}} \right) \right]^2} \times \sum_1^{38} \sigma^2 \left( \frac{q_{i,j}}{\Delta h_{i,j}} \right) =$$

$$\left[ \frac{q_{i,j}}{\Delta h_{i,j}} \right]^2 \times \frac{k_t^2}{\left[ \sum_1^{38} \left( \frac{q_{i,j}}{\Delta h_{i,j}} \right) \right]^2} \times \sum_1^{38} \left( \frac{q_{i,j}}{\Delta h_{i,j}} \right)^2$$

$$\left[ \begin{array}{l} \sigma_r^2 q_{i,j} \\ + \left( \frac{\partial h_{ou,i,j}}{\partial t_{ou,i,j}} \right)^2 \frac{\sigma^2 t_{ou,i,j}}{\Delta h_{ou,i,j}^2} \end{array} \right] \left\{ \begin{array}{l} \text{term due to the} \\ \text{power} \\ \text{term due to the} \\ \text{outlet temperature} \end{array} \right.$$

(2.13)

$$\left[ + \left( \frac{\partial h_{in,i,j}}{\partial t_{in,i,j}} \right)^2 \frac{\sigma_{t_{in,i,j}}^2}{\Delta h_{in,i,j}^2} \right] \left\{ \begin{array}{l} \text{term due to the} \\ \text{inlet temperature.} \end{array} \right.$$

(2.13)  
(continued)

The above derivation assumes that the coolant stays subcooled and the evaluation of  $\sigma_h$  can be obtained from:

$$\sigma_h^2 = \left[ \frac{\partial h}{\partial t} \right]^2 \sigma_t^2 \quad . \quad (2.14)$$

A code called FLOFA II has been written to compute the same information as FLOFA I (see 2.3.1) with the effective flow factors obtained from the enthalpy rise. (see Appendix B).

### 2.3.3 Evaluation of Uncertainties

In order to calculate the uncertainties associated with the effective flow factors, it is necessary to have the values of the control instrument uncertainties (thermocouples, flux detectors). Research done in this area showed that very little data exists.

### Thermocouples:

The assembly exit thermocouple is made with Chromel-Alumel. This type of thermocouple has a good resistance to radiation damage and has a characteristic curve which stays linear with time (6)(7)(8). However the accuracy of this type is not very good. The standards of the American National Standard Institute require that the thermocouple manufacturers meet the following specification for the Chromel-Alumel type:

- for temperatures between 0 and 530°F
  - limits of errors of standard thermocouple  $\pm 4^\circ\text{F}$
  - limits of errors of special thermocouple  $\pm 2^\circ\text{F}$
- for temperatures above 530°F
  - limits of errors of standard thermocouple  $\pm 0.75\%$
  - limits of errors of special thermocouple  $\pm 0.375\%$

However these standards do not indicate the confidence level associated with these values of possible errors. In fact this gives only a value of the thermocouple uncertainty due to the reading accuracy. Other values of uncertainty need to be found concerning:

- calibration error,
- gamma heating of the hot junction,

- hot junction drift due to nuclear permutations,
- hot junction position with respect to the center of the fuel assembly.

A study done for the San Onofre Reactor (9) gives some numerical values for the different uncertainties:

- calibration error (statistical) evaluated as  $\pm 0.3^{\circ}\text{F}$  which is due to the fact that the isothermal calibration of the thermocouples is done at an average temperature of  $530^{\circ}\text{F}$  which is about  $40^{\circ}\text{F}$  below the operating temperatures of the thermocouples (a check on the calibration curve of the thermocouples shows that the correction at  $530^{\circ}\text{F}$  is the same at  $570\text{-}580^{\circ}\text{F}$ ). This calibration error is used to take into account also a possible human error and is conservative in that respect,
- gamma heating (non-statistical) evaluated as  $+ 0.5^{\circ}\text{F}$  to take into account absorption of gamma rays energy by the hot junction at full power which gives higher readings,
- hot junction drift due to nuclear permutations (non-statistical) evaluated as  $+1^{\circ}\text{F}$ . The records concerning the thermocouples off-sets for Connecticut Yankee

Reactor between two isothermal calibrations, show a maximal drift of 1.55°F in Core III (1.75°F in Core IV) and also show that these drifts may occur in opposite directions, which indicates that this error is of a non-statistical character,

- hot junction position with respect to the fuel assembly (statistical) evaluated as  $\pm 3^\circ\text{F}$ . This tends to take into account the fact that the coolant temperature at the plane where the temperature is taken, is not uniform,
- reading accuracy (statistical) evaluated as  $\pm 2.0^\circ\text{F}$  due to the instrumentation.

The vessel inlet temperature of the coolant is measured by a precision platinum resistance temperature bulb in each loop. This type of instrument can be used in this case because the hot junction is not exposed to the full neutron flux and the exposure damage is less in this case than for the exit thermocouples. Based on the engineering experience, it is common to consider an inaccuracy of  $\pm 0.2^\circ\text{F}$  associated with the reading of such RTD (Resistor Temperature Device).



### Power Distribution:

The movable miniature flux detectors are supposed to give their signal with a  $\pm 2.0\%$  accuracy and Westinghouse estimated the accuracy of the power map on the order of  $\pm 5\%$  (10). Both values are related to a two sigma confidence level.

#### 2.3.4 Results of the Sensitivity Analysis

At the time the sensitivity analysis was developed, the uncertainties associated with the control instruments were not known with enough precision, and the standard deviations of the effective flow factors were calculated with assumed values for these uncertainties, based on engineering experience and judgment.

The results obtained assumed for the one sigma confidence level:

- relative standard deviation of the power: 0.0275
- standard deviation of the outlet temperature:  $2.50^{\circ}\text{F}$
- standard deviation of the inlet temperature:  $0.10^{\circ}\text{F}$

For the one sigma confidence level the relative standard deviation of the effective flow factor was in the range 4.5 - 7.0%, and was an inverse function of the coolant temperature rise in the fuel assembly. The rela-

tive standard deviation of the effective flow factor is also strongly influenced by the standard deviation of the outlet temperature as it can be seen on Table 2. Table 2 gives the breakdown of the standard deviation of the effective flow factor and the comparison between the two types of analysis ( $C_p$  temperature dependent and independent).

#### 2.4 Physical Meaning of the Effective Flow Factors

If no cross flow between the assemblies is assumed, it is obvious that in this case the effective flow factor is the same as the normalized inlet flow distribution. But the real case of PWR is more complex and the assumption of no cross flow does not necessarily hold.

The energy equation can be written as:

$$\begin{aligned}
 & C_p (m_{in,i,j} + \Delta m_{i,j}) t_{ou,i,j} - C_p m_{in,i,j} t_{in,i,j} \\
 & = Q_{i,j} - C_p \Delta m_{i,j} t_{1,i,j} \quad . \quad (2.15)
 \end{aligned}$$

where  $t_1$  represents the effective temperature for the energy due to the cross flow exchange,  $C_p \Delta m t_{1,i,j}$ .

Type of case	$C_p = \text{constant}$	$C_p = f(T)$
Four components due to:		
- normalization factor	2.60 %	2.61 %
- power	23.38 %	30.09 %
- outlet temperature	73.91 %	67.17 %
- inlet temperature	<u>0.11 %</u>	<u>0.13 %</u>
	100.00 %	100.00 %

Three total contributions due to:

- power	24.00 %	30.88 %
- outlet temperature	75.87 %	68.97 %
- inlet temperature	<u>0.13 %</u>	<u>0.15 %</u>
	100.00 %	100.00 %

Table 2 Breakdown of the Standard Deviation of the Effective Flow Factor for BOC in Core III of Connecticut Yankee Reactor

Solving for  $m_{in,i,j}$  we obtain:

$$m_{in,i,j} = \frac{Q_{i,j}/C_p - \Delta m_{i,j}(t_{l,i,j} + t_{ou,i,j})}{t_{ou_{ij}} - t_{in_{ij}}} \quad (2.16)$$

And if these ratios are normalized over the area of instrumented assemblies:

$$EFF_{i,j} = \frac{\frac{Q_{i,j}}{C_p} - \Delta m_{i,j}(t_{l,i,j} + t_{ou,i,j})}{t_{ou_{ij}} - t_{in_{ij}}} \times \frac{38}{\sum_I m_{in,i,j}} \quad (2.17)$$

A similar equation can be derived for the case where the heat capacity of the coolant is assumed to be temperature dependent. The evaluation of the term corresponding to the energy exchange between the assembly  $i,j$ , with its neighbors can be reduced to a net energy exchange which corresponds to a cross flow exchange and thermal mixing. It is rather difficult to evaluate this net energy exchange,

because it implies knowledge of the temperature or enthalpy distribution along the fuel assemblies and also an idea where the cross flow exchange takes place. One way to get the feeling for this process is to run calculations with a thermal hydraulic code like COBRA III C which yields the temperature enthalpy axial flow and cross flow of the coolant. Results of this type of analysis will be presented in Chapter 3.

## CHAPTER 3

### POWER DISTRIBUTION CALCULATIONS AND USE OF THE CODE "INCORE"

#### 3.1 Introduction

The power distribution and the corresponding peaking factors  $F_H^N$ ,  $F_q^N$ ,  $F_q$ , are calculated by the code INCORE.

This code uses as main inputs:

- the flux detectors readings measuring the axial flux in the assemblies instrumented with an in-core thimble, and the flux at each thimble location,
- the prediction of the core wide power distribution and flux thimble obtained from the code PDQ<sup>(11)</sup>, in which the results of depletion calculations using the code LEOPARD<sup>(12)</sup>, are fed.

In the Connecticut Yankee core there are two flux detectors which can be moved within all of the 18 flux thimbles located in 18 different assemblies.

The power distribution calculations using the computer code PDQ, is generally done stepwise each 2,000 MWD/MTU.

Some of the INCORE results are used to determine the:

- maximum linear heat generation rate and its location,
- average linear heat generation rate,
- peaking factors and their locations,
- effective flow factors.

### 3.2 Purpose of the Calculation

A sensitivity analysis has been developed for the code INCORE for two purposes:

- it was found interesting to know the sensitive effect of the major inputs on the results, since no information so far, was not readily available on this type of analysis,
- the sensitivity analysis is needed for good information on the accuracy of the results of the power distribution calculations from the knowledge of the inputs accuracies.

The code INCORE is a proprietary code from Westinghouse, and information beyond input and output is not included in this study.

### 3.3 Modification of the Major Inputs

As mentioned in 3.2, because of the proprietary character of INCORE, no numerical values relative directly to the inputs or outputs are given in this work. But to understand what has been done, some explanations are given how the inputs have been treated.

The sensitivity analysis has been developed from the variation of:

- flux detectors readings given by the movable incore flux detectors,

- PDQ flux predictions of the flux at the flux thimble locations,
- power distribution prediction given by the PDQ code, for hot channel and assembly.

This study, of course, uses numerical values of the inputs for a given cycle, at a given time in the cycle, however the time effect has been considered. The parameters were varied one at a time, to see their corresponding effect on the entire output.

### 3.3.1 Variation of the Flux Detector Readings

For a given thimble, the detectors readings have been varied by the same factor (5% increase has been used to be sure of having enough variation in the outputs without too much distortion of the power pattern).

It has been verified for the first thimble, that an increase and a decrease of the flux detector readings by the same factor, would give output changes equal in absolute value. This was done to check that the change was small enough to be considered a linear effect.

### 3.3.2 Variation of the Flux Thimble Information

This part of the sensitivity study was treated in a very similar fashion as for the flux detectors readings. For a given thimble, both the thermal flux information and the fast flux information, were varied by the same factor



(5% increase has been used for the same reasons as 3.2.1, after having verified the linearity of the changes in the outputs with the changes in the inputs).

### 3.3.3 Variation of the Predicted Power

The sensitivity analysis for this part has been conducted in a different way, because for a given cycle the power distribution changes only with time. Therefore, comparisons have been done between collection of power predictions at BOC, MOC and EOC of CORE III.

## 3.4 Results of the Sensitivity Study

The results of this study depend upon the kind of input that has been varied. The results are presented in a relative value, expressing the percentage change in the assemblies for a change of one percent in a given location for a given type of input. To handle the calculation of the variations, a code VARY has been written and all the details are given in Appendix B. All the results have been summarized in curves for easy use.

### 3.4.1 Variation of the Flux Detectors Readings

The increase of the flux detector readings in a given flux thimble, gives the following results:

- $F_{\Delta H}^N$ ,  $F_q^N$  are increased locally by variable amounts depending on the relative position of the assemblies with respect to the location where the increase takes place:

- for the assembly in which the increase is made,  $F_{\Delta H}^N$ ,  $F_q^N$  are increased by almost the same amount (1% increase of the flux detector readings gives 0.9% increase for  $F_{\Delta H}^N$  and  $F_q^N$ ),
- for the assemblies immediately surrounding the assembly where the increase is made,  $F_{\Delta H}^N$ ,  $F_q^N$  are increased by amounts depending on the relative position of the assemblies (they may share one side with the assembly where the increase is done, or just share a corner), and are found to be a function of the distance from the center of the core,
- $F_{\Delta H}^N$ ,  $F_q^N$  are decreased throughout the rest of the core by a fairly constant amount,
- $F_z$  is unchanged.

Figure 7 summarizes the results of flux detector, giving the relative variation of  $F_{\Delta H}^N$  or  $F_q^N$  normalized to a percent increase in the flux detectors readings as a function of the radial position of the assembly from the center of the core and as a function of the position in which the increase in the flux detector readings takes place.

Key to Fig. 7a, 7b, 9a, 9b

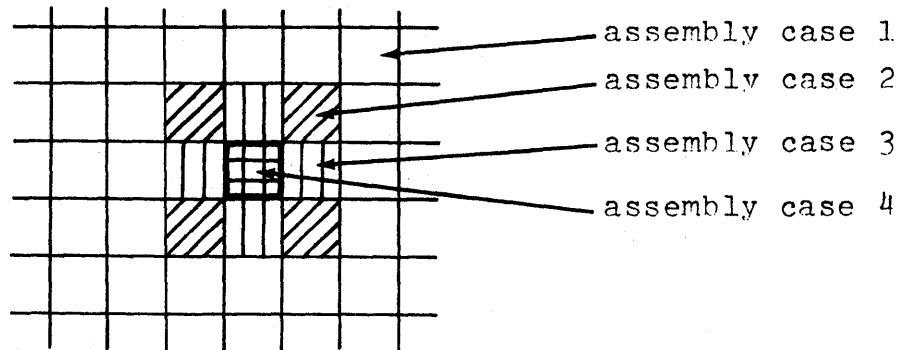
Curve A = relative variation of the peaking factors for the assemblies which are not the neighbors of the assemblies where the variation (flux detector readings or flux thimble prediction) is done, (assembly case 1)

Curve B = relative variation of the peaking factors for the assemblies sharing a common corner with the assemblies where the variation is done, (assembly case 2)

Curve C = relative variation of the peaking factors for the assemblies sharing a common side with the assemblies where the variation is done, (assembly case 3)

Curve D = relative variation of the peaking factors for the assemblies where the variation is done, (assembly case 4).

Radiale distance from core center = distance between the center of an assembly and the center of the assembly H 8.



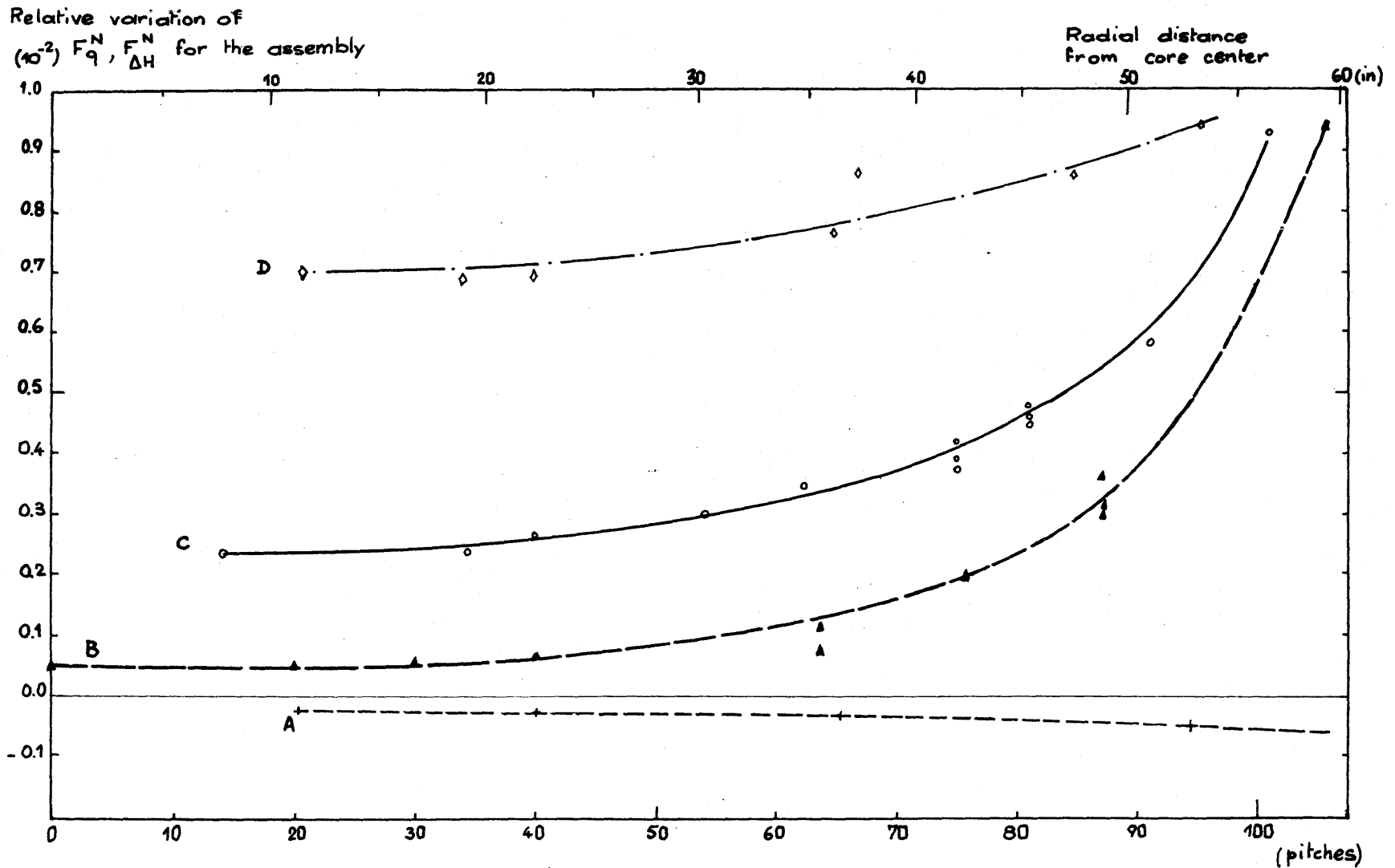


Fig. 7a Relative variation of  $F_q^N, F_{\Delta H}^N$  for 1% increase in the flux detector readings.  
 Assembly averaged values.

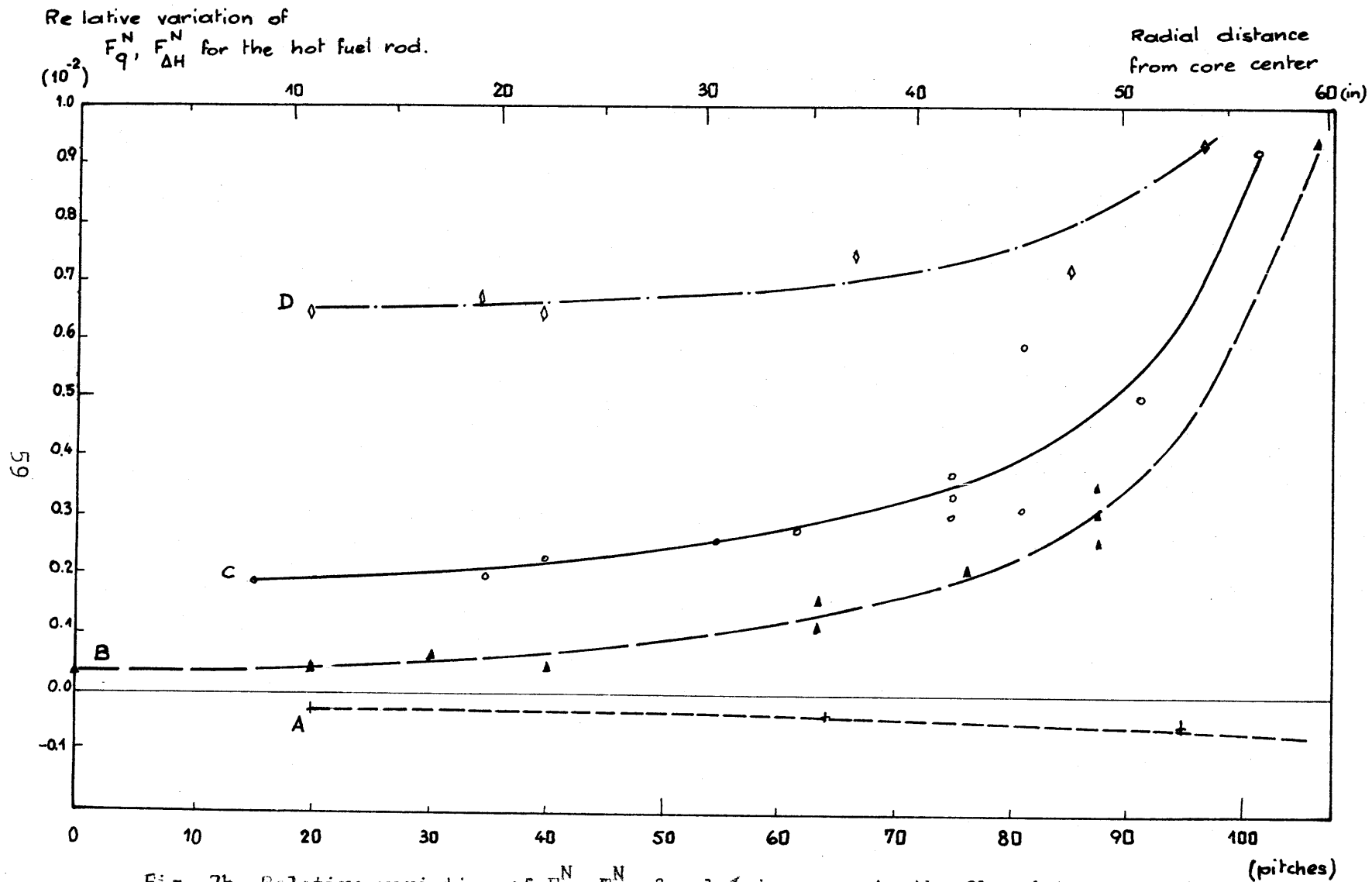


Fig. 7b Relative variation of  $F_q^N, F_{\Delta H}^N$  for 1% increase in the flux detector readings. Hot fuel rods values.

As an example, an increase in the flux detector reading of 1% in assembly M10 (radial distance = 67.08 pitches) leads to:

- increase of  $F_{\Delta H}^N$  or  $F_q^N$  of: 0.42 in N 10 (radial distance = 80.78 pitches, sharing one common side with M 10, curve B)
- 0.32 in N 11 (radial distance = 87.46 pitches sharing one common corner with M 10, curve C).

Now it should be mentioned that INCORE computes the power distribution from the flux detector readings, and the number of thimbles used for the calculation of the power in a given assembly, apparently may vary from 1 to several thimbles.

It has been found that the curves of Fig. 7 are time independent for a given core, a given assembly has its power changing with burn-up, however the relative variation of  $F_{\Delta H}^N$  or  $F_q^N$  stays constant while burn-up increases.

Some of the calculated relative variations of  $F_{\Delta H}^N$  or  $F_q^N$  may not behave as shown in Fig. 7. This is apparently due to the way INCORE treats the problem and it

has been found that the calculated power is inferred from the information related to a fairly far thimble as shown in Fig. 8. For this case there has been a one percent increase in the flux detector readings in M 12 and the corresponding variation in N 12 should be 0.73 according to Fig. 7, but instead it is - 0.028 corresponding to the variation of the rest of the core. This is due to the fact that the power in N 12 is given from the information in L 5, which in this case does not see the effect of the one percent increase in M 12.

#### 3.4.2 Variation of the Flux Thimble Prediction

Very similar results have been obtained for this part as in 3.3.1, except that in this case the variations of  $F_{\Delta H}^N$  and  $F_q^N$  are in the opposite direction to the way they varied in 3.3.1.

The increase of the flux thimble prediction in a given thimble, gives the following results:

- $F_{\Delta H}^N$ ,  $F_q^N$  are decreased locally by variable amounts depending on the relative position of the assemblies with respect to the location where the increase takes place:

- for the assembly where the increase is done,  $F_{\Delta H}^N$ ,  $F_q^N$  are decreased by almost the same amount,

VARIATION OF FCN AND FCMA FOR A VARIATION OF IC E-03 IN CASE # CCB

	15	14	13	12	11	10	9	8	7	6	5	4	3	2	1	
R																***** *-0.251 -C.26C -0.275* *-C.260 -0.260 -0.245*
																VARIATION OF DETECTORS READINGS
P																***** *-0.258 -C.266 -C.268 -0.264 -0.272 -0.278 -0.262* *-C.272 -C.277 -C.266 -0.273 -0.259 -0.272 -0.292* *****
																VARIATION OF FCMA IN ASSEMBLY #12
N																***** UNITS = 1.0 E-03 *-0.289  2.584 -C.277 -C.273 -C.258 -0.279 -0.273 -0.270 -0.289* *-0.279  2.554 -0.278 -C.276 -C.274 -C.26C -0.263 -0.265 -0.279* *****
M																***** * 9.645  8.657  3.084 -C.271 -C.269 -0.279 -0.268 -0.269 -0.265 -0.263 -0.267* * 9.742  8.735  3.372 -C.259 -C.259 -C.26C -C.277 -0.261 -0.257 -0.266 -0.278* *****
L																***** *-0.253  3.627  3.454  0.585 -C.271 -C.266 -C.261 -C.263 -0.265 -0.277 -0.280 -0.269 -0.260* *-0.254  3.626  3.466  0.565 -C.267 -C.264 -0.276 -C.266 -0.266 -0.277 -0.275 -0.264 -0.261* *****
K																***** *-0.266 -C.281 -0.267 -0.268 -0.255 -C.268 -0.277 -C.263 -0.265 -0.265 -0.268 -0.267 -0.272* *-0.266 -C.280 -0.275 -C.265 -C.272 -C.269 -C.260 -0.255 -0.253 -0.265 -0.277 -0.277 -0.264* *****
J																***** *-0.277 -0.274 -C.270 -C.264 -0.263 -0.264 -C.271 -C.261 -0.252 -0.259 -0.257 -0.273 -0.272 -0.278 -0.271* *-0.273 -0.275 -C.27C -0.271 -C.27A -C.264 -0.259 -C.273 -C.280 -0.265 -0.276 -0.278 -0.268 -0.267 -0.266* *****
H																***** *-0.275 -0.270 -0.264 -0.271 -C.265 -0.252 -C.258 -C.271 -0.258 -0.267 -0.258 -0.270 -0.268 -0.275 -0.272* *-0.277 -C.272 -C.267 -0.266 -0.266 -0.257 -C.271 -0.274 -0.270 -0.274 -0.258 -0.268 -0.271 -C.263 -0.271* *****
G																***** *-0.277 -0.269 -C.265 -0.267 -0.276 -C.276 -C.269 -0.261 -0.252 -0.263 -0.277 -0.273 -0.272 -0.278 -0.271* *-0.273 -C.270 -0.281 -C.272 -C.274 -C.281 -C.26C -C.273 -C.28C -C.267 -0.278 -0.278 -0.268 -0.267 -0.266* *****
F																***** *-0.265 -0.261 -0.269 -0.266 -0.266 -0.266 -0.276 -0.267 -0.268 -0.269 -0.258 -0.267 -0.272* *-0.264 -0.271 -0.259 -0.284 -C.270 -C.267 -C.262 -0.271 -0.273 -0.267 -0.262 -0.277 -0.264* *****
E																***** *-0.234 -C.270 -C.267 -0.261 -0.269 -C.264 -0.257 -C.267 -0.255 -0.291 -0.269 -0.273 -0.287* *-0.239 -0.279 -0.274 -0.275 -0.267 -C.281 -C.27C -C.264 -0.270 -0.275 -0.277 -0.266 -0.263* *****
D																***** *-0.263 -C.264 -C.28C -C.27C -C.26C -0.267 -0.26C -0.273 -0.269 -0.267 -0.271* *-0.277 -C.265 -C.272 -C.259 -C.275 -C.255 -C.275 -0.280 -0.276 -0.268 -0.254* *****
C																***** *-0.267 -C.271 -C.26C -C.268 -0.263 -0.268 -0.26C -0.261 -0.251* *-0.277 -C.264 -0.265 -C.259 -C.275 -0.259 -0.265 -0.267 -0.281* *****
B																***** *-0.263 -C.266 -C.263 -0.270 -C.263 -0.266 -0.265* *-0.262 -0.275 -C.261 -0.252 -C.261 -0.275 -0.265* *****
A																***** *-C.259 -C.264 -0.259* *-C.277 -C.262 -0.277* *****

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Fig. 8 Typical example of assembly power not behaving as the general rule.



- for the assemblies immediately surrounding the assembly where the increase is done,  $F_{\Delta H}^N$ ,  $F_q^N$  are decreased by amounts depending on the relative position of the assemblies and are functions of the distance from the center of the core,
- $F_{\Delta H}^N$ ,  $F_q^N$  are increased throughout the rest of the core by a fairly constant amount,
- $F_z$  is unchanged.

Figure 9 summarizes the results for this second part of the sensitivity study, giving the relative variation of  $F_{\Delta H}^N$ ,  $F_q^N$  for one percent increase of the flux thimble prediction as a function of the radial position of the assembly from the center of the core and as a function of the position where the increase in the flux thimble prediction takes place.

The same remarks concerning the way to compute the relative variation in a given assembly from the variations generated by the individual assemblies used to compute the power in that assembly, are still applicable.

It has been found that the curves of Fig. 8 are time independent for a given core.

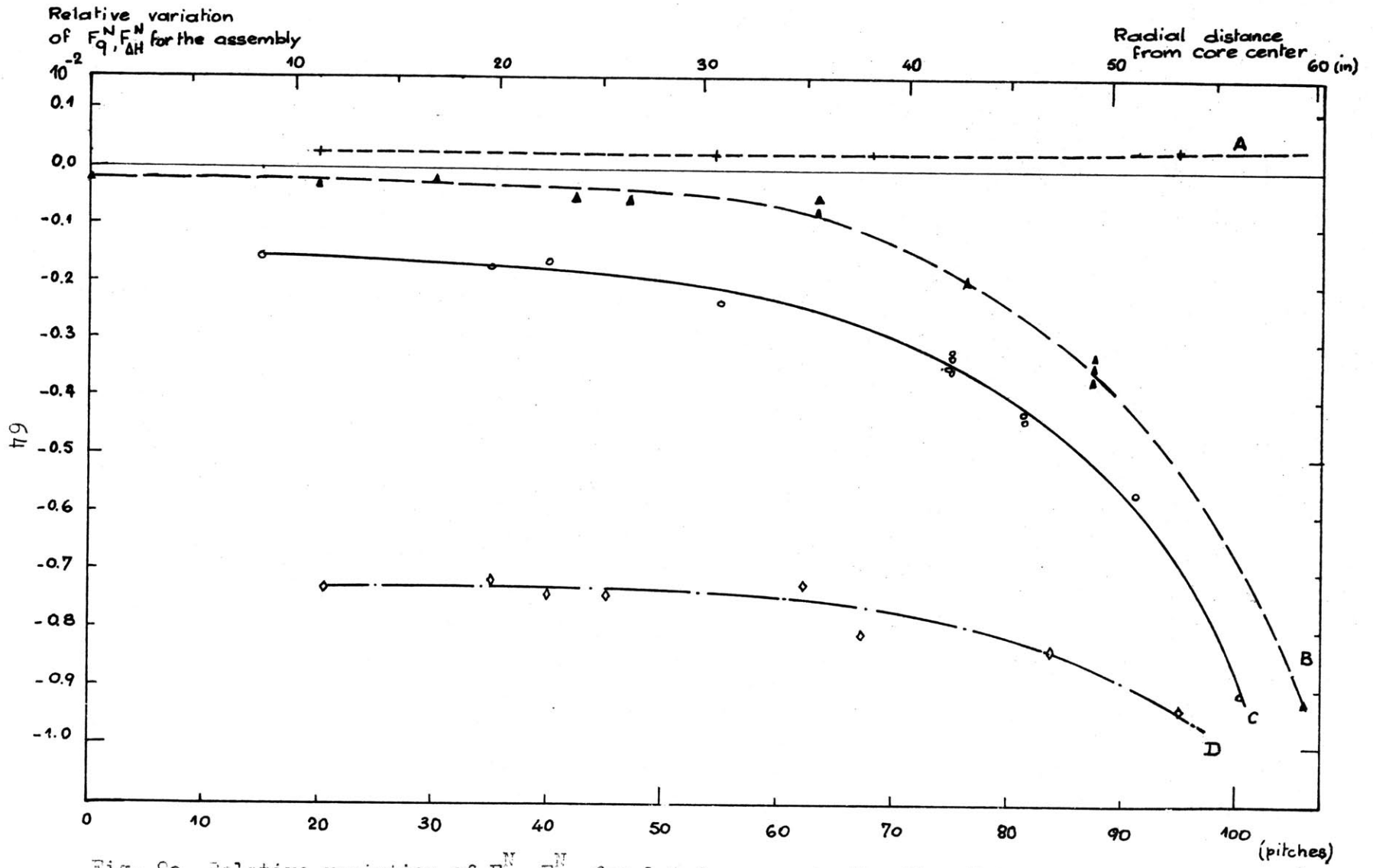


Fig. 9a Relative variation of  $F_Q^N, F_{\Delta H}^N$  for 1% increase in the flux thimble prediction. Assembly averaged values.

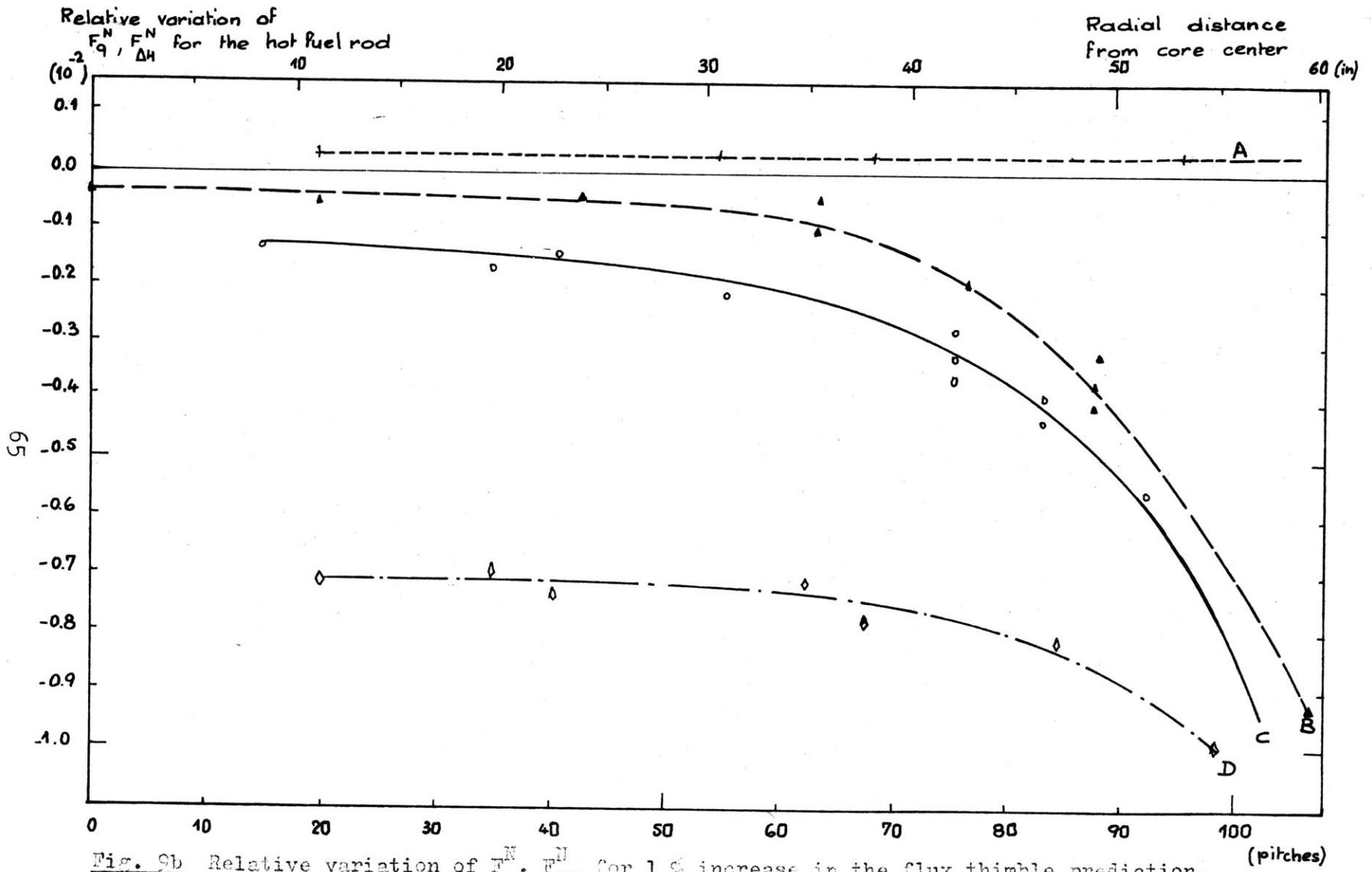


Fig. 9b Relative variation of  $F_q^N, F_{\Delta H}^N$  for 1% increase in the flux thimble prediction. Hot fuel rods values.

### 3.4.3 Variation of the Predicted Power

The relative variation of the calculated values for  $F_{\Delta H}^N$ ,  $F_q^N$  compared to the relative variation of the predicted values for these two quantities is in the ratio of one.

An increase of one percent in the predicted power in any assembly produces an increase of one percent of the calculated power for that assembly.

### 3.4.4 Combined Variations

The relative variation of  $F_{\Delta H}^N$ ,  $F_q^N$  in a given assembly can be obtained from the relative variations in this assembly due to:

- the detector uncertainty,
- the flux thimble prediction uncertainty,
- the power prediction uncertainty,

and combine these uncertainties with each of the thimbles used for the computation of the power in this assembly.

It would be conservative to say that the relative variation is roughly the sum of each individual relative variations in this given assembly, and since these uncertainties are independent, they can properly be combined statistically.

### 3.4.5 Uncertainties Values

The uncertainty of the flux detector is simple to evaluate, it is given by the detector manufacturer specifications:  $\pm 1.0\%$  for one sigma confidence level (2)(10).

The uncertainty in the flux thimble prediction or the uncertainty of the predicted power cannot be evaluated easily. Since the flux thimble and the power predictions come from PDQ, it would be necessary to develop a sensitivity analysis on the PDQ code as a function of the various inputs. It can be assumed, based on engineering experience and judgment, that the flux thimble uncertainty and the predicted power uncertainty (for the hot channel and the assemblies) are in the order of 4% for one sigma confidence level.

## CHAPTER 4

### FLOW CALCULATIONS AND USE OF THE CODE "COBRA III C"

#### 4.1 Application of "COBRA III C" to the Connecticut Yankee Case

In Chapter 2 the possible importance of the cross flow pattern was noted. This cross flow distribution can be predicted by some thermal hydraulic analysis codes, the choice was oriented to the latest version of COBRA III C <sup>(13)</sup>, because of its availability. Most of the reactor vendors have established very sophisticated codes for thermal hydraulic calculations, most of these codes are, however, classified as proprietary information.

The latest version of the COBRA code presents an improved modeling of the transverse momentum equation, including temporal and spatial acceleration of the diversion cross flow. The code can handle steady state and transients calculations for:

- enthalpy, temperature, pressure drop of the fluid,
- axial flow and diversion cross flow,
- fuel and clad temperatures,
- heat flux and critical heat flux ratio.

The original version <sup>(13)</sup> is written to accommodate:

- 15 subchannels,

- 25 fuel rods,
- 30 subchannel connections,
- 2 types of fuel.

The main idea in using COBRA III C lies in the fact that a code written for subchannel thermal hydraulic analysis can be used to treat a problem dealing with:

- flow regions which may represent either subchannels or lumped subchannels (all the subchannels of a fuel assembly may be lumped in one flow region) or a combination of both types of subchannels and lumped subchannels,
- fuel regions which may represent either a fuel rod or lumped fuel rods (all the fuel rods of a fuel assembly may be lumped in one fuel region) or a combination of both types of fuel rods and lumped fuel rods.

This approach allows representation of a rather large fraction of the reactor core without losing the detailed information on some selected subchannels, for instance the hottest subchannels and the hottest fuel rod. This type of analysis can work either way:

- several assemblies can be lumped together and consider only the detailed analysis of the hottest subchannels in the core,

- treat the hottest subchannel in each assembly individually and lump the rest of the subchannels in each assembly. In this case, regions of different assemblies would not be lumped. Therefore in general for the same core, more flow regions would be defined in this approach than the above approach.

The trade-off stands between the computation time and size required in the computer to solve the problem, and the degree of detailed analysis desired.

The choice for this work was to treat an octant of the core, using the assembly as the unit flow region, except for the hottest assembly, where the four subchannels surrounding the hottest fuel rod were treated as four separate flow regions, and the rest of the fuel assembly was lumped into one flow region. This allowed the calculation of the values of:

- minimum DNBR and its location,
- maximum fuel center line temperature and its location,
- maximum clad surface temperature and its location.

#### 4.2 Changes Made in "COBRA III C"

The original version of COBRA III C did not allow the treatment of the Connecticut Yankee case as it is



described in 4.1. Some necessary changes have been made such as:

- the maximum number of flow regions has been increased from 15 to 30,
- the maximum number of fuel regions has been increased from 15 to 30,
- the number of connected flow regions has been increased from 30 to 47,
- the number of nodes for the axial heat flux distribution has been increased from 30 to 39 (to allow the use of the axial heat flux distribution given by INCORE = 35 nodes + 4 nodes for the two ends of the fuel rod),
- the axial node number has been reduced from 60 to 30, since an axial node length of 6 inches seems to be optimal (precision of the results does not increase for smaller axial node length, see later the sensitivity analysis).

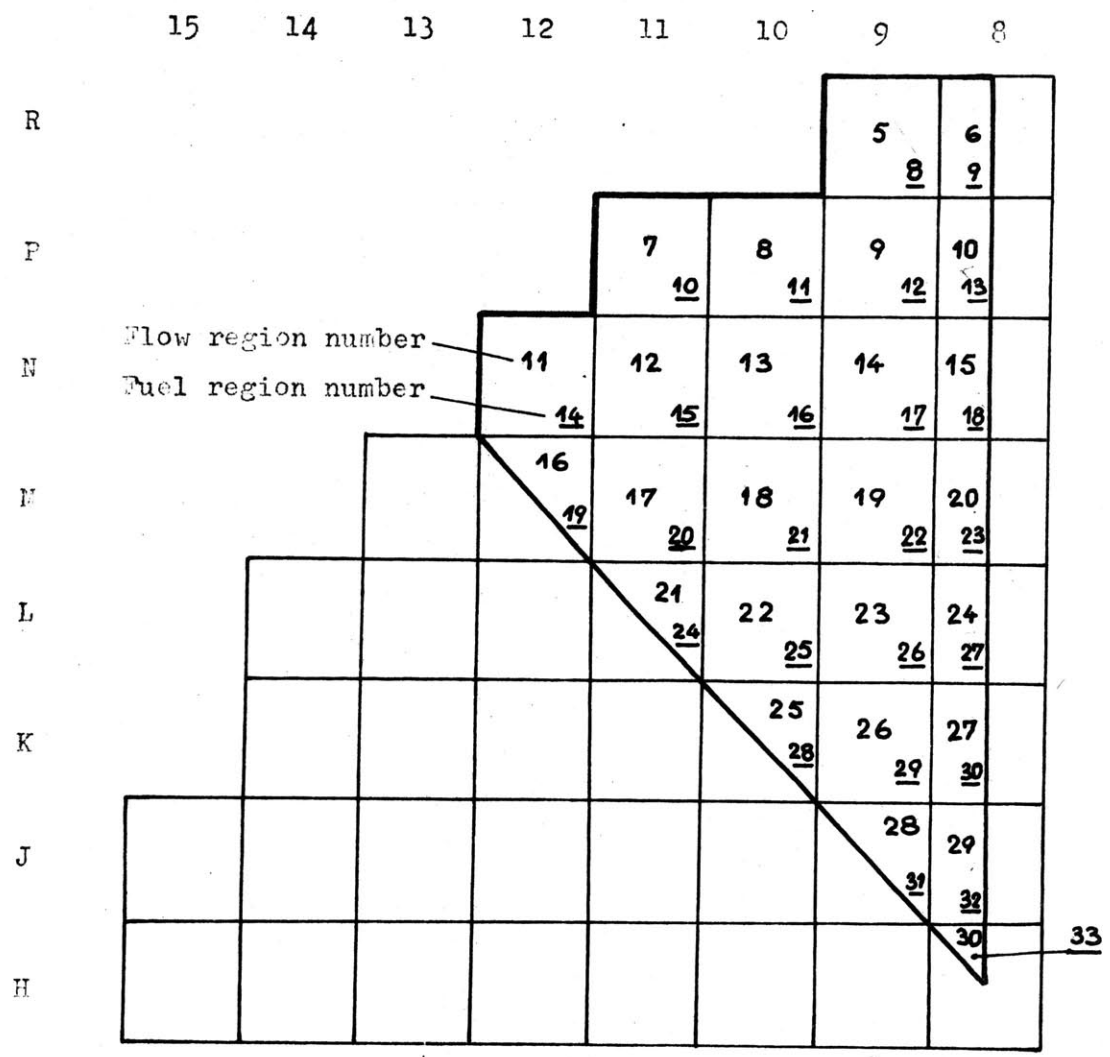
The axial number can be reduced in order to save space in the computer, however the reduction may be too important in some cases, especially when this affects the axial node length<sup>(14)</sup>.

This work deals only with steady state calculations, but the transients part of the original version has been kept for a possible use. Appendix C lists the changes made and tells how new changes can be handled as a function of the parameters changed (flow region number, fuel region number, fuel type number, etc.).

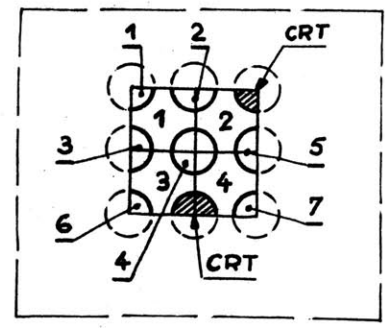
#### 4.3 Connecticut Yankee Model

As mentioned in 4.1, the code COBRA III C once modified, has been applied to the octant of the Connecticut Yankee Reactor containing the hottest fuel assembly. The calculations were done for a given power distribution obtained from INCORE, corresponding to the beginning of cycle III. Figure 10 shows how the core octant was modeled.

It was assumed that there was no net cross flow across the boundaries of the octant. One may argue with this assumption and say that the net cross flow through the boundary is not zero. But the cross flow represents only few percents of the axial flow and as it will be seen later on in the sensitivity analysis, the assembly exit conditions (temperature and axial flow) are not strong functions of the amount of cross flow. Therefore, this assumption even if not completely true, can be



CRT = Control rod  
thimble (water  
hole)



Detail of the hot  
fuel rod surrounded  
by four subchannels  
in the hot assembly  
( N 11 )

Fig. 10 Model of the Connecticut  
Yankee to be used in a COBRA III C  
calculation.

taken without introducing large errors on the entire results. However, it would not be a good assumption if the hottest channel were located very close to the boundary, or even if the hottest fuel assembly were split by the boundary. In this case it would be necessary to change the pattern for the model, and perhaps consider a quadrant of the core instead of the octant.

It is obvious also that the only rigorous solution would be to treat the entire core and this would allow a solution to the problem of any assymetry existing in the core, but this is a too expensive solution for the point-of-view of computation.

#### 4.4 Input Deck

A sample input deck is given in Appendix B, however a few remarks are given in order to explain how different types of flow regions such as subchannels and assemblies (or lumped assemblies) can be used under a common node of computation.

The geometry of the flow region has to be described as it is physically for either a subchannel or for lumped subchannels. In that respect the hydraulic diameter of the flow region will keep a physical meaning. It is also important to input the real diameter of the fuel rods, to have a model which stays consistent with the flow region geometry and allows realistic fuel temperatures calculations.

The power generated in a particular fuel region deposited in a given flow region can be determined by using the following rules:

- Power from the hottest fuel rod to the hot channel:

$$f_P = f_G \times \frac{1}{\alpha} \times \frac{1}{F_q^N} \times F_{\Delta H}^{\text{stat}}, \quad (4.1)$$

where:

$$F_{\Delta H}^{\text{stat}} = \frac{F_{\Delta H}^E}{F_{LP} \times F_R \times F_M}, \quad (4.2)$$

(see Ref. 15)

- Power from the hottest rod to other flow regions:

$$f_P = f_G \times \frac{1}{\alpha} \times \frac{1}{F_q^N}, \quad (4.3)$$

- Power from other fuel regions to the hot channel:

$$f_P = f_G \times \frac{1}{\alpha} \times F_{\Delta H}^{\text{stat}}, \quad (4.4)$$

- Power from other fuel regions to other flow regions:

$$f_p = f_G \times \frac{1}{\alpha} \quad , \quad (4.5)$$

- Power from lumped fuel rods to lumped subchannels:

$$f_p = \frac{1}{\alpha} \times N_{rod} \quad . \quad (4.6)$$

The detailed instructions concerning how to set up the data deck can be found in front of the COBRA III C deck. The options selected to treat the Connecticut Yankee case are listed below:

- friction factor correlation:

$$f = 0.184 \text{ Re}^{-0.2} \quad (15) \quad , \quad (4.7)$$

- subcooled void correlation: Levy correlation,
- bulk void correlation: homogeneous model,
- two phase friction multiplier: homogeneous model,
- wall viscosity correction to the friction factor included,
- spacer pressure losses included,
- subcooled mixing correlation: Rowe correlation (16)

$$\beta = 0.0062 \frac{D}{S} \text{ Re}^{-0.1} \quad , \quad (4.8)$$

- two phase mixing correlation: same as the subcooled mixing correlation,
- no thermal conduction mixing assumed,

for the rest of the details of the data deck, see the sample input in Appendix B.

#### 4.5 Sensitivity Study

Some of the input parameters to COBRA III C, such as the cross flow resistance factor, turbulent momentum factor, S/L parameter defining the control volume\*, are not very easy to estimate or to measure. Some measurements of the cross flow resistance factor have been done<sup>(17)</sup> but they are related to particular conditions which do not correspond to this case. It was decided to develop a sensitivity study, of the selected parameters, and see how sensitive the results are sensitive to the choice of these parameters. In addition, the results of this sensitivity analysis are used to optimize the computation between the precision of the results and the computation time.

This sensitivity study has been performed on the following parameters:

-----

\* (where S is the gap spacing between fuel regions and L the length of the control volume, see Ref. 13)

- axial node length, using node lengths of 7.9, 6.0, 4.2 in.,
- flow convergence factor, using factors of 0.020, 0.010, 0.005,
- S/L parameter for the control volume, using values of 0.10, 0.25, 0.50,
- turbulent momentum factor, using values of 0.0, 0.5, 0.9,
- cross flow resistance factor, using values of 0.1, 0.5, 0.9.

The best set of values to be used for the Connecticut Yankee Reactor is the set which has been used in the reference case.

#### 4.6 Results of the Sensitivity Analysis

##### 4.6.1 General Remarks

It is important to keep in mind that the results are valid for the calculational model used to represent the Connecticut Yankee Reactor and it would probably be unwise to generalize on these results to all the PWR's without any further checks on other reactors.

It has been found that the assembly exit conditions of the coolant are not greatly affected by the values chosen for each parameter. Some differences exist as far



as computation time is concerned, and therefore the choice of each parameter can, in general, be established for minimum computation time.

#### 4.6.2 Results

For each type of sensitivity study, two figures are used to summarize the results. These figures give:

- assembly exit temperature of the coolant,
- normalized flow distribution of the coolant at the assembly exit.

In addition, Table 5 lists the comparison of the following computed parameters for each case:

- minimum DNBR and its axial location from the inlet,
- maximum fuel center line temperature and its location,
- maximum clad temperature and its location,
- core pressure drop and hot channel pressure drop,
- number of iterations required to obtain the flow solution,
- computation time.

Table 3 lists the possible bounds of the parameters used for this study and the physical significants of these limits. Table 4 gives the correspondence between the case numbers and the type of variation done in each case.

Figures 11 through 20 summarize the comparison of the

Parameters	Bounds of Parameters mini/maxi	Physical Significance
Axial node length	number of nodes = 2 node separation = 126.7 in. number of nodes = 30 node separation = 4.23 in.	node 1 at core inlet node 2 at core outlet (depends on code conditions)
Flow convergence factor	no bounds	in (%) represents the allowed derivation between axial mass flow rates between two iterations
S/L parameter	0                      1	corresponds to the volume through which cross flow exchange is calculated
Turbulent momentum factor	0                      1	accounts for imperfect analogy between eddy diffusivity of heat and momentum
Cross flow resistance factor	0                      1	k = 0    no cross flow resistance k = 1    full cross flow resistance

Table 3    Physical Significance and Bounds on the Parameters Used  
In the Sensitivity Study on COBRA III C

Case No.	Type of Varied Parameter	Value of the Parameter
1	Reference case	
2	Axial node length	7.919 in.
1	Axial node length (ref. case)	6.023 in.
3	Axial node length	4.223 in.
4	Flow convergence factor	0.020
1	Flow convergence factor (ref. case)	0.010
5	Flow convergence factor	0.005
6	S/L parameter	0.10
1	S/L parameter (ref. case)	0.25
7	S/L parameter	0.50
8	Turbulent momentum factor	0.0
1	Turbulent momentum factor (ref. case)	0.5
9	Turbulent momentum factor	0.9
10	Cross flow resistance factor	0.1
1	Cross flow resistance factor (ref. case)	0.5
11	Cross flow resistance factor	0.9
12	Forced inlet flow distribution	-
13	Equal pressure gradient at the inlet	-
14	Uniform mass flux at the inlet	-

Table 4 Correspondence Between the Case Numbers and the Type of Sensitivity Study Done

	15	14	13	12	11	10	9	8	
R							562.20	565.72	1
							562.19	565.75	2
							562.16	565.74	3
							-	573.8	4
<b>Hottest assembly= N 11</b>									
P					564.64	579.03	588.61	571.86	
					564.62	579.05	588.65	571.91	
					564.55	579.01	588.63	571.96	
					571.6	575.7	588.2	-	
N				567.53	591.74	574.82	579.04	579.31	
				567.52	591.76	574.89	579.11	579.35	
				567.44	591.70	574.95	579.13	579.36	
				572.2	-	578.5	576.4	574.3	
M					581.37	587.59	586.51	586.45	574.54
					581.39	587.66	586.56	586.50	574.50
					581.34	587.68	586.56	586.51	574.70
					582.7	583.7	577.8	583.9	-
L						575.61	576.79	577.43	582.64
						575.72	576.88	577.53	582.63
						575.80	576.93	577.59	582.61
						575.1	575.3	576.6	578.7
K							583.58	584.31	570.29
							583.63	584.37	570.50
							583.64	584.38	570.50
							574.5	-	-
J								574.28	579.31
								574.38	579.32
								574.39	579.38
								572.2	579.4
H									567.80
									567.90
									567.89
									567.9

- 1: Calculated value for axial node length=7.9in.  
( case n° 2 )
- 2: Calculated value for axial node length=6.0in.  
( reference case )
- 3: Calculated value for axial node length=4.2in.  
( case n° 3 )
- 4: Measured value (From outlet thermocouple)

595.03	591.62
595.10	591.69
-	-
591.80	591.18
591.87	591.28
591.88	591.32
-	-

**Fig. 11** Comparison of outlet temperatures as a function of axial node length.

**Hot subchannels**

	15	14	13	12	11	10	9	8	
R							1.0069	1.0062	1
							1.0063	1.0058	2
							1.0059	1.0059	3
									4
<b>Hottest assembly= N 11</b>									
P					1.0057	0.9978	0.9929	1.0047	
					1.0051	0.9974	0.9927	1.0044	
					1.0044	0.9974	0.9931	1.0049	
N				1.0039	0.9909	1.0031	1.0000	0.9997	
				1.0034	0.9906	1.0029	1.0000	0.9997	
				1.0027	0.9906	1.0033	1.0000	1.0003	
M					0.9982	0.9940	0.9951	1.0065	
					0.9980	0.9940	0.9952	1.0066	
					0.9979	0.9945	0.9959	1.0064	
L						1.0027	0.9993	1.0021	0.9981
						1.0028	0.9996	1.0024	0.9986
						1.0033	1.0000	1.0026	0.9986
K							0.9975	1.0072	
							0.9980	1.0076	
							0.9982	1.0068	
J							1.0045	1.0009	
							1.0050	1.0015	
							1.0040	1.0000	
H								1.0098	
								1.0098	
								1.0098	

- 1: Calculated value for axial node length=7.9 in.  
( case n° 2 )
- 2: Calculated value for axial node length=6.0 in.  
( reference case )
- 3: Calculated value for axial node length=4.2 in.  
( case n° 3 )
- 4: -

0.9935	0.9785
0.9934	0.9781
0.9935	0.9780
0.9784	0.9790
0.9781	0.9786
0.9780	0.9784

**Fig. 12** Comparison of the normalized outlet flow distribution as a function of the axial node length.

**Hot subchannels**

	15	14	13	12	11	10	9	8	
R							562.19	565.75	1
							562.19	565.75	2
							562.23	565.79	3
							-	573.8	4
<b>Hottest assembly- N 11</b>									
P					564.62	579.05	588.65	571.91	
					564.62	579.05	588.65	571.91	
					564.68	579.11	588.73	571.93	
					571.6	575.7	588.2	-	
N				567.52	591.76	574.89	579.11	579.35	
				567.52	591.76	574.89	579.11	579.35	
				567.57	591.10	574.88	579.11	579.37	
				572.2	-	578.5	576.4	574.3	
M					581.39	587.66	586.56	586.50	574.65
					581.39	587.66	586.56	586.50	574.65
					581.50	587.67	586.59	586.51	574.57
					582.7	583.7	577.8	583.9	-
L						575.72	576.88	577.53	582.63
						575.72	576.88	577.53	582.63
						575.62	576.82	577.46	582.68
						575.1	575.3	576.6	578.7
K							583.63	584.37	570.50
							583.63	584.37	570.50
							583.63	584.35	570.33
							574.5	-	-
J								574.38	579.32
								574.38	579.32
								574.30	579.31
								572.2	579.4
H									567.50
									567.90
									567.82
									567.9

- 1: Calculated value for flow convergence factor  
PCF = 0.020 ( case n° 4 )
- 2: Calculated value for flow convergence factor  
PCF = 0.010 ( reference case )
- 3: Calculated value for flow convergence factor  
PCF = 0.005 ( case n° 5 )
- 4: Measured value (From outlet thermocouple)

595.10	591.69
595.10	591.69
595.16	591.74
-	-
591.87	591.28
591.87	591.28
591.93	591.33
-	-

**Fig. 13** Comparison of outlet temperatures as a function of the flow convergence factor.

**Hot subchannels**

	15	14	13	12	11	10	9	8	
R							1.0063	1.0058	1
							1.0063	1.0058	2
							1.0074	1.0064	3
									4
<u>Hottest assembly- N 11</u>									
P					1.0051	0.9974	0.9927	1.0044	
					1.0051	0.9974	0.9927	1.0044	
					1.0064	0.9979	0.9927	1.0046	
N				1.0034	0.9906	1.0029	1.0000	0.9997	
				1.0034	0.9906	1.0029	1.0000	0.9997	
				1.0046	0.9908	1.0030	0.9998	0.9995	
M					0.9980	0.9940	0.9952	0.9954	1.0066
					0.9980	0.9940	0.9952	0.9954	1.0066
					1.0012	0.9938	0.9947	0.9947	1.0062
L						1.0028	0.9996	1.0024	0.9986
						1.0028	0.9996	1.0024	0.9986
						1.0026	0.9992	1.0018	1.0030
K							0.9980	0.9980	1.0076
							0.9980	0.9980	1.0076
							0.9981	0.9975	1.0073
J								1.0059	1.0015
								1.0059	1.0015
								1.0059	1.0013
H									1.0098
									1.0098
									1.0098

- 1: Calculated value for flow convergence factor  
FCF = 0.020 ( case n° 4 )
- 2: Calculated value for flow convergence factor  
FCF = 0.010 ( reference case )
- 3: Calculated value for flow convergence factor  
FCF = 0.005 ( case n° 5 )
- 4: -

0.9934	0.9781
0.9934	0.9781
0.9932	0.9781
0.9781	0.9786
0.9781	0.9786
0.9781	0.9790

**Fig. 14** Comparison of the normalized outlet flow distribution as a function of the flow convergence factor.

Hot subchannels

	15	14	13	12	11	10	9	8			
R							562.20	565.80	1		
							562.19	565.75	2		
							562.27	565.76	3		
							-	573.8	4		
P							564.70	579.05	588.73	571.98	
							564.62	579.05	588.65	571.91	
							564.72	579.06	588.60	571.90	
							571.6	575.7	588.2	-	
N							567.45	591.87	574.93	579.12	579.37
							567.52	591.76	574.89	579.11	579.35
							567.61	591.71	574.88	579.11	579.36
							572.2	-	578.5	576.4	574.3
M							581.44	587.65	586.57	586.50	574.63
							581.39	587.66	586.56	586.50	574.65
							581.39	587.65	586.57	586.51	574.60
							582.7	583.7	577.8	583.9	-
L							575.67	576.86	577.51	582.63	582.63
							575.72	576.88	577.53	582.63	582.63
							575.66	576.85	577.50	582.71	582.71
							575.1	575.3	576.6	578.7	578.7
K							583.68	584.35	570.19	570.19	570.19
							583.63	584.37	570.50	570.50	570.50
							583.66	584.39	570.29	570.29	570.29
							574.5	-	-	-	-
J							574.25	579.43	579.43	579.43	579.43
							574.38	579.32	579.32	579.32	579.32
							574.33	579.40	579.40	579.40	579.40
							572.2	579.4	579.4	579.4	579.4
H								567.72	567.72	567.72	567.72
								567.90	567.90	567.90	567.90
								567.84	567.84	567.84	567.84
								567.90	567.90	567.90	567.90

Hottest assembly- N11

- 1: Calculated value for parameter S/L = 0.10  
( case n° 6 )
- 2: Calculated value for parameter S/L = 0.25  
( reference case )
- 3: Calculated value for parameter S/L = 0.50  
( case n° 7 )
- 4: Measured value (From outlet thermocouple)

595.12	591.71
595.10	591.69
595.09	591.67
-	-
591.90	591.30
591.87	591.28
591.85	591.26
-	-

Fig. 15 Comparison of outlet temperatures as a function of the S/L parameter.

Hot subchannels



	15	14	13	12	11	10	9	8	
R							1.0069	1.0066	1
							1.0063	1.0058	2
							1.0069	1.0064	3
									4
<b>Hottest assembly- N 11</b>									
P					1.0054	1.0001	0.9935	1.0054	
					1.0051	0.9974	0.9927	1.0044	
					1.0057	0.9979	0.9932	1.0048	
N				1.0036	0.9910	1.0038	0.9999	1.0005	
				1.0034	0.9906	1.0029	1.0000	0.9997	
				1.0039	0.9912	1.0032	1.0001	0.9998	
M					0.9983	0.9947	0.9959	1.0068	
					0.9980	0.9940	0.9952	1.0066	
					0.9984	0.9942	0.9951	1.0063	
L						1.0034	0.9998	1.0022	0.9978
						1.0028	0.9996	1.0024	0.9986
						1.0027	0.9993	1.0019	0.9980
K							0.9975	0.9970	1.0055
							0.9980	0.9980	1.0076
							0.9974	0.9973	1.0066
J							0.9993	0.9968	
							1.0050	1.0015	
							1.0037	1.0002	
H								1.0053	
								1.0098	
								1.0108	

- 1: Calculated value for parameter  $S/L = 0.10$   
( case n° 6 )
- 2: Calculated value for parameter  $S/L = 0.25$   
( reference case )
- 3: Calculated value for parameter  $S/L = 0.50$   
( case n° 7 )
- 4: -

0.9935	0.9783
0.9934	0.9781
0.9935	0.9783
0.9783	0.9787
0.9781	0.9786
0.9783	0.9788

**Fig. 16** Comparison of the normalized outlet flow distribution as a function of the  $S/L$  parameter.

**Hot subchannels**

	15	14	13	12	11	10	9	8	
R							562.19	565.75	1
							562.19	565.75	2
							562.19	565.75	3
							-	573.8	4
P					564.62	579.05	588.67	571.91	
					564.62	579.05	588.65	571.91	
					564.62	579.05	588.67	571.91	
					571.6	575.7	588.2	-	
N					567.51	591.78	574.88	579.10	579.37
					567.52	591.76	574.89	579.11	579.35
					567.51	591.79	574.88	579.10	579.37
					572.2	-	578.5	576.4	574.3
M					581.40	587.67	586.58	586.52	574.61
					581.39	587.66	586.56	586.50	574.65
					581.40	587.67	586.58	586.52	574.61
					582.7	583.7	577.8	583.9	-
L					575.69	576.86	577.52	582.68	
					575.72	576.88	577.53	582.63	
					575.69	576.86	577.52	582.68	
					575.1	575.3	576.6	578.7	
K						583.65	584.38	570.41	
						583.63	584.37	570.50	
						583.65	584.38	570.41	
						574.5	-	-	
J							574.37	579.36	
							574.38	579.32	
							574.37	579.36	
							572.2	579.4	
H								567.88	
								567.90	
								567.88	
								567.9	

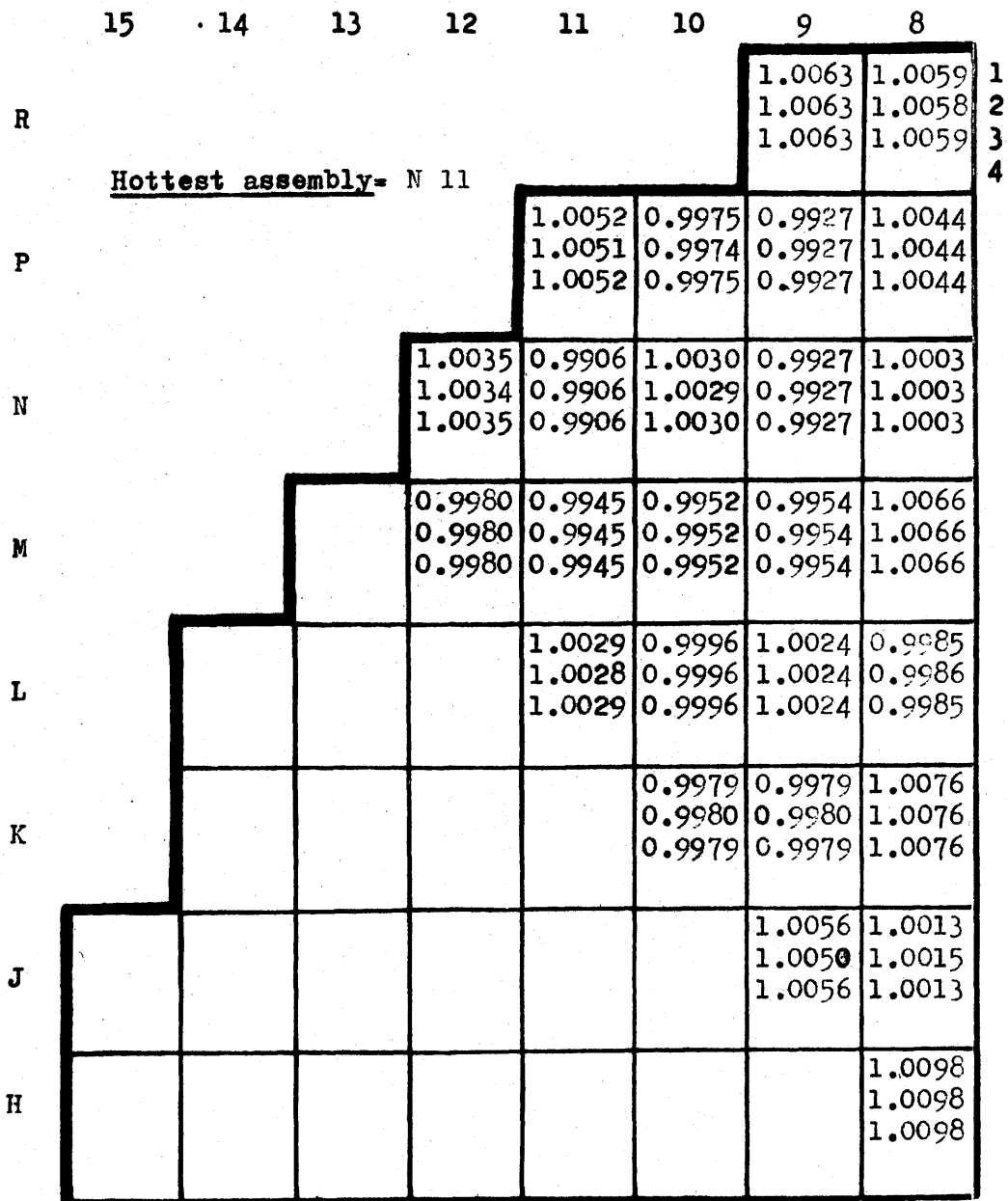
Hottest assembly = N 11

- 1: Calculated value for turbulent momentum factor  $TMF = 0.5$  ( reference case )
- 2: Calculated value for turbulent momentum factor  $TMF = 0.0$  ( case n° 8 )
- 3: Calculated value for turbulent momentum factor  $TMF = 0.9$  ( case n° 9 )
- 4: Measured value (From outlet thermocouple)

595.17	591.59
595.10	591.69
595.22	591.54
-	-
591.78	591.18
591.87	591.28
591.73	591.12
-	-

Fig. 17 Comparison of outlet temperatures as a function of the turbulent momentum factor.

Hot subchannels



Hottest assembly- N 11

- 1: Calculated value for turbulent momentum factor  $TMF = 0.5$  ( reference case )
- 2: Calculated value for turbulent momentum factor  $TMF = 0.0$  ( case n° 8 )
- 3: Calculated value for turbulent momentum factor  $TMF = 0.9$  ( case n° 9 )
- 4: -

0.9935	0.9781
0.9934	0.9781
0.9935	0.9781
0.9781	0.9786
0.9781	0.9786
0.9781	0.9786

Fig. 18 Comparison of the normalized outlet flow distribution as a function of the turbulent momentum factor.

Hot subchannels

	15	14	13	12	11	10	9	8	
R							562.19	565.75	1
							562.19	565.75	2
							562.19	565.75	3
							-	573.8	4
<b><u>Hottest assembly= N 11</u></b>									
P					564.62	579.05	588.65	571.91	
					564.62	579.05	588.65	571.91	
					564.62	579.05	588.65	571.91	
					571.6	575.7	588.2	-	
N									
					567.52	591.76	574.89	579.11	579.35
					567.52	591.76	574.89	579.11	579.35
					567.52	591.76	574.89	579.11	579.35
M									
					572.2	-	578.5	576.4	574.3
					581.39	587.66	586.56	586.50	574.65
					581.39	587.66	586.56	586.50	574.65
L									
					581.39	587.66	586.56	586.50	574.65
					582.7	583.7	577.8	583.9	-
					575.72	576.88	577.53	582.63	
K									
					575.72	576.88	577.53	582.63	
					575.72	576.88	577.53	582.63	
					575.1	575.3	576.6	578.7	
J									
							583.63	584.37	570.50
							583.63	584.37	570.50
							583.63	584.37	570.50
H									
							574.5	-	-
							574.38	579.32	
							574.38	579.32	
						574.38	579.32		
						572.2	579.4		
							567.91		
							567.91		
							567.91		
							567.9		

- 1: Calculated value for cross flow resistance  
K = 0.1 ( case n° 10 )
- 2: Calculated value for cross flow resistance  
K = 0.5 ( reference case )
- 3: Calculated value for cross flow resistance  
K = 0.9 ( case n° 11 )
- 4: Measured value (From outlet thermocouple)

595.09	591.68
595.10	591.69
595.10	591.69
-	-
591.87	591.28
591.87	591.28
591.87	591.28
-	-

**Fig. 19** Comparison of outlet temperatures as a function of the cross flow resistance.

**Hot subchannels**

	15	14	13	12	11	10	9	8	
R							1.0063	1.0058	1
							1.0063	1.0058	2
							1.0063	1.0058	3
									4
					<u>Hottest assembly- N 11</u>				
P					1.0051	0.9974	0.9927	1.0044	
					1.0051	0.9974	0.9927	1.0044	
					1.0051	0.9974	0.9927	1.0044	
N				1.0034	0.9906	1.0029	1.0000	0.9997	
				1.0034	0.9906	1.0029	1.0000	0.9997	
				1.0034	0.9906	1.0029	1.0000	0.9997	
M				0.9980	0.9940	0.9952	0.9954	1.0066	
				0.9980	0.9940	0.9952	0.9954	1.0066	
				0.9980	0.9940	0.9952	0.9954	1.0066	
L					1.0028	0.9996	1.0024	0.9986	
					1.0028	0.9996	1.0024	0.9986	
					1.0028	0.9996	1.0024	0.9986	
K						0.9980	0.9980	1.0076	
						0.9980	0.9980	1.0076	
						0.9980	0.9980	1.0076	
J							1.0050	1.0015	
							1.0050	1.0015	
							1.0050	1.0015	
H								1.0098	
								1.0098	
								1.0098	

- 1: Calculated value for cross flow resistance  
K = 0.1 ( case n° 10 )
- 2: Calculated value for cross flow resistance  
K = 0.5 ( reference case )
- 3: Calculated value for cross flow resistance  
K = 0.9 ( case n° 11 )
- 4: -

0.9934	0.9781
0.9934	0.9781
0.9934	0.9781
0.9781	0.9786
0.9781	0.9786
0.9781	0.9786

**Fig. 20** Comparison of the normalized outlet flow distribution as a function of the cross flow resistance.

Hot subchannels

results obtained for the sensitivity study where the different parameters listed above have been varied for the same coolant distribution at the core inlet (equal pressure gradient in all the flow regions).

This part of the sensitivity study has been done by using the inlet flow distribution given by the subroutine SPLIT, which splits the flow to get the same pressure gradient at the core inlet. It assumed that there is no spatial acceleration component of pressure drop <sup>(13)</sup>. It is recalled that COBRA III C allows the use of three possible options for the flow inlet distribution:

- same mass flux everywhere at the core inlet,
- same pressure gradient at the core inlet,
- forced inlet distribution at the core inlet <sup>(18)</sup>.

By using the reference values of parameters, the three inlet flow distributions were tested against each other. Figures 21 through 24 and Table 5 summarize the results of this comparison.

Figure 25 gives a comparison of the axial mass flux and the diversion cross flow for the hot channel as a function of the flow inlet distribution. Figure 26 gives a plot of the mass flux in the hot assembly and in the assembly at the center of the core.

	15	14	13	12	11	10	9	8	
R							562.18	565.97	1
							562.19	565.75	2
							562.20	566.00	3
							-	573.8	4
P					564.61	579.05	588.63	571.88	
					564.62	579.05	588.65	571.91	
					564.63	579.05	588.67	571.92	
					571.6	575.7	588.2	-	
N					567.52	591.75	574.88	579.12	579.32
					567.52	591.75	574.89	579.11	579.35
					567.51	591.82	574.88	579.13	579.37
					572.2	-	578.5	576.4	574.3
M					581.37	587.66	586.53	586.48	574.64
					581.39	587.66	586.56	586.50	574.65
					581.45	587.67	586.59	586.53	574.59
					582.7	583.7	577.8	583.9	-
L					575.73	576.89	577.55	582.63	
					575.72	576.88	577.53	582.63	
					575.61	576.84	577.49	582.76	
					575.1	575.3	576.6	578.7	
K						583.60	584.33	570.30	
						583.63	584.37	570.50	
						583.69	584.38	570.12	
						574.5	-	-	
J							574.46	579.43	
							574.38	579.32	
							574.36	579.51	
							572.2	579.4	
H								567.90	
								567.90	
								567.81	
								567.9	

Hottest assembly- N 11

- 1: Forced inlet distribution.  
( case n° 12 )
- 2: Equal pressure gradient distribution.  
( case n° 13 )
- 3: Uniform mass flux distribution.  
( case n° 14 )
- 4: Measured value (From outlet thermocouple)

595.09	591.68
595.10	591.69
595.05	591.67
-	-
591.87	591.28
591.87	591.28
591.57	591.12
-	-

Fig. 21 Comparison of outlet temperatures as a function of the inlet distribution.

Hot subchannels

	15	14	13	12	11	10	9	8	
R							1.0129	1.0118	1
							1.0150	0.9017	2
							-0.0021	0.1101	3
									4
<u>Hottest assembly- N 11</u>									
P					1.0081	1.0007	0.9967	1.0081	
					0.9634	0.9737	0.9327	0.8915	
					0.0447	0.0270	0.0640	0.1166	
N				1.0053	0.9918	1.0040	1.0011	1.0014	
				1.0150	0.9532	1.0040	0.8917	0.9632	
				-0.0097	0.0386	0.0000	0.1094	0.0382	
M					0.9986	0.9939	0.9942	0.9944	1.0024
					1.0967	1.0560	0.9122	0.9942	1.0658
					-0.0981	-0.0621	0.0820	0.0002	-0.0634
L						1.0007	0.9995	0.9987	0.9958
						0.9632	1.0350	0.9737	1.1377
						0.0375	-0.0355	0.0250	-0.1419
K							0.9936	0.9933	1.0026
							1.0248	1.0970	1.1987
							-0.0312	-0.1037	-0.1961
J								0.9991	0.9959
								0.9940	1.1067
								0.0051	-0.1108
H									1.0037
									1.0850
									-0.0823

1: Normalized outlet distribution.

2: Normalized inlet distribution.

3: Difference between outlet and inlet distributions.

4: -

0.9937	0.9805
0.9532	0.9533
0.0405	0.0272
0.9804	0.9810
0.9533	0.9510
0.0271	0.0300

Fig. 22 Flow distributions for the forced inlet distribution case ( case n° 12 ). Hot subchannels





	15	14	13	12	11	10	9	8	
R							1.0068	1.0063	1
							1.0001	0.9998	2
							0.0067	0.0065	3
									4
<b>Hottest assembly- N 11</b>									
P					1.0055	0.9978	0.9931	1.0048	
					1.0001	1.0001	1.0001	0.9998	
					0.0054	-.0023	-.0032	0.0050	
N					1.0038	0.9909	1.0032	1.0003	0.9998
					1.0001	1.0001	1.0001	1.0001	0.9998
					0.0037	-.0092	0.0031	0.0002	0.0000
M									
					0.9982	0.9942	0.9952	0.9953	1.0036
					0.9998	1.0001	1.0001	1.0001	0.9998
L									
					1.0028	1.0024	1.0020	0.9980	
K									
J									
H									

- 1: Normalized outlet distribution.
- 2: Normalized inlet distribution.
- 3: Difference between outlet and inlet distributions.
- 4: -

0.9937	0.9786
1.0000	1.0000
-.0063	-.0214
0.9784	0.9790
1.0000	1.0000
-.0216	-.0210

**Fig. 24** Flow distributions for the uniform mass flux inlet distribution case ( case n° 14 ).

**Hot subchannels**

Key to Table 5:

- A: Case number (see Table 4 for the type of study done)
- B: Minimum DNBR
- C: Location of the MDNBR from the inlet (in.)
- D: Maximum fuel centerline temperature ( $^{\circ}\text{F}$ )
- E: Location of the maximum fuel centerline temperature from inlet (in)
- F: Maximum clad outside temperature ( $^{\circ}\text{F}$ )
- 97 G: Location of the maximum clad outside temperature from inlet (in)
- H: Core pressure drop (psi)
- I: Hot channel pressure drop (psi)
- J: Number of iterations to obtain the flow solution
- K: Computation time - CPU time - (sec)

NOTE: All the values of the MDNBR are related to fuel rod No. 4 facing the subchannel No. 1. All the temperatures (fuel centerline and clad outside) are related to the fuel rod No. 4.

A	B	C	D	E	F	G	H	I	J	K
1	3.891	90.5	2724.9	54.3	637.1	96.5	19.55	19.53	2	89.558
2	3.895	95.0	2723.8	55.4	636.8	95.0	19.55	19.53	2	69.417
3	3.888	92.9	2725.2	54.9	637.4	97.1	19.54	19.51	2	124.886
4	3.891	90.5	2724.9	54.3	637.1	96.5	19.54	19.52	2	89.558
5	3.887	90.5	2724.9	54.3	637.1	96.5	19.54	19.52	3	132.296
6	3.891	90.5	2724.9	54.3	637.1	96.5	19.55	19.52	2	89.258
7	3.891	90.5	2724.9	54.3	637.1	96.5	19.55	19.53	2	89.245
8	3.881	90.5	2724.9	54.3	636.9	96.5	19.55	19.53	2	91.581
9	3.876	90.5	2724.9	54.3	636.9	96.5	19.55	19.53	2	91.688
10	3.891	90.5	2724.9	54.3	637.1	96.5	19.54	19.51	2	89.558
11	3.891	90.5	2724.9	54.3	637.1	96.5	19.55	19.51	2	89.279
12	3.876	90.5	2724.9	54.3	637.1	96.5	19.55	19.45	4	183.902
13	3.891	90.5	2724.9	54.3	637.0	96.5	19.55	19.53	2	92.723
14	3.890	90.5	2724.9	54.3	637.1	96.5	19.55	19.55	2	95.060

Table 5 Summary of the Results of the Sensitivity Analysis on COBRA 3C

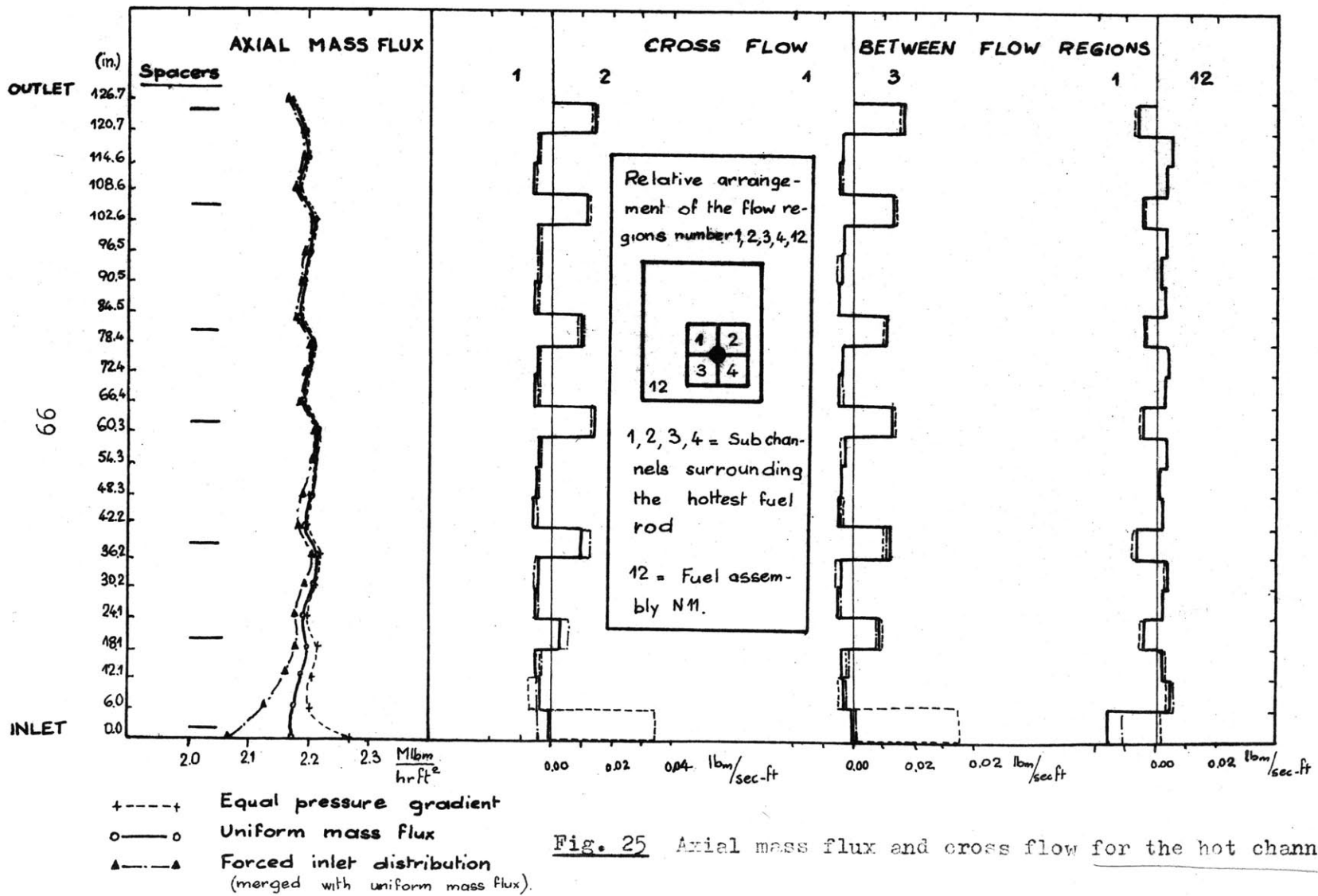


Fig. 25 Axial mass flux and cross flow for the hot channel.

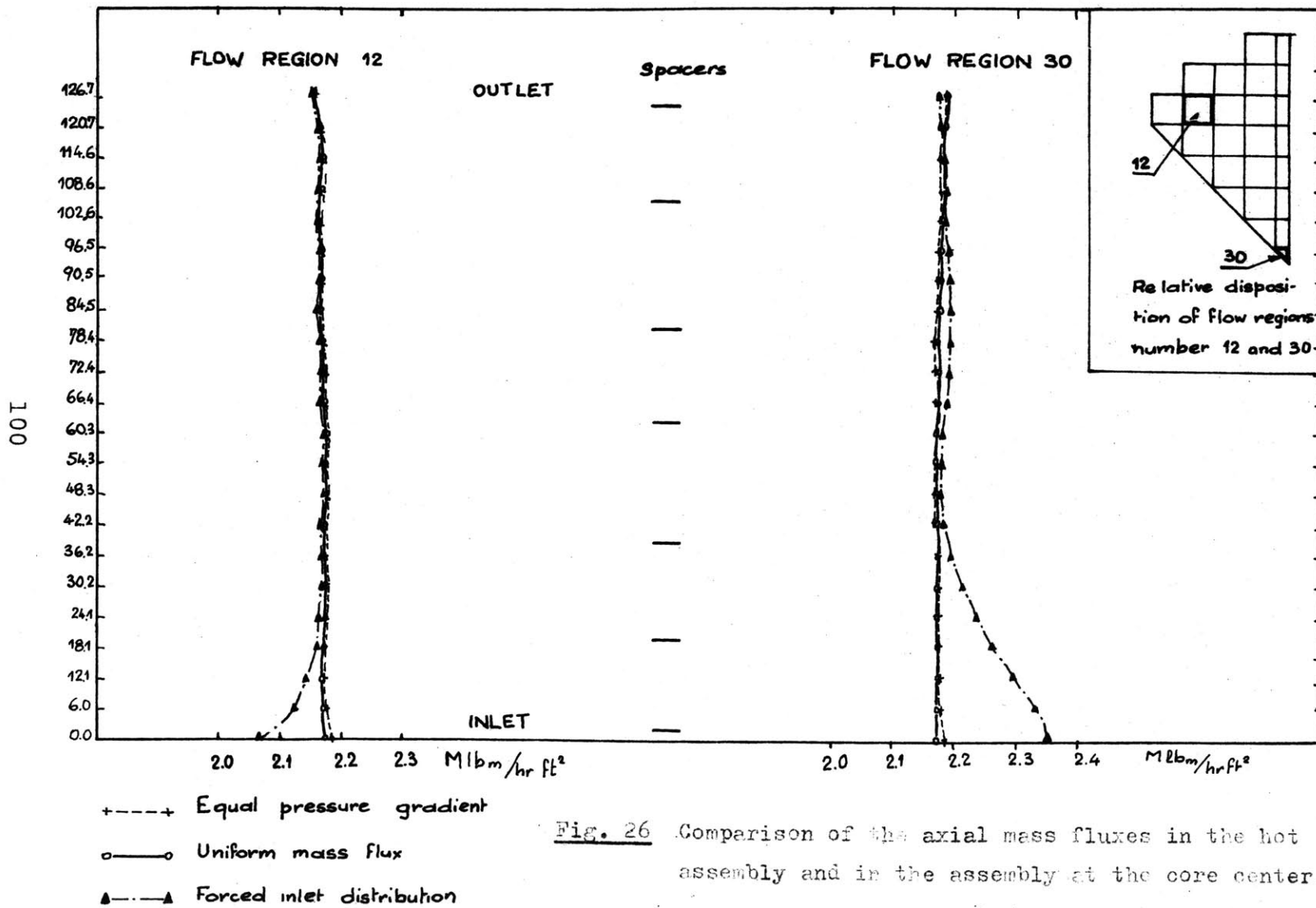


Fig. 26 Comparison of the axial mass fluxes in the hot assembly and in the assembly at the core center.

#### 4.6.3 Conclusions Given by the Sensitivity Study

A general remark can be made concerning the outlet conditions for each assembly:

- the assembly outlet conditions (axial flow, temperature) are not very sensitive to either the different parameters used for the computation, or the inlet flow distribution.

In particular the cross flow resistance factor has very little effect on the flow distribution at the outlet, but of course the cross flow pattern inside of the core depends on this cross flow resistance factor.

As stated it would be probably unwise to generalize these results to all the PWR, but it should be mentioned that very similar results have been obtained from a sensitivity study done with COBRA III C on the Yankee Rowe Reactor (19).

From Figure 25 and 26 it appears that the inlet flow distribution does not effect the outlet conditions and the coolant seems to perform a self-redistribution leading to achievement of an equilibrium distribution after 2 to 4 feet from the core inlet.

However this study shows that the use of the values of a measured inlet flow distribution (18) is not very advantageous, since it tends to introduce a flow instability

in the computation increasing the computation time without any increase in the accuracy of the results. This inlet flow distribution is related to measurements taken on a seventh scale model and correspond to isothermal conditions.

The best inlet distribution suitable for this model is probably the distribution given by the use of the pressure gradient option, since it represents a reduction of the axial flow in the hot channel and an increase of the axial flow in the neighboring channels, as opposed to the uniform mass flux case where the axial flow is reduced in all the channels in the hot zone.

#### 4.7 Validity of the Model

It was implicitly assumed that the Connecticut Yankee Reactor is highly subcooled when the options in COBRA III C were chosen. It is possible to check where the subcooled boiling occurs by predicting the location of incipient nucleation from available correlation. Three correlations were investigated: Bergles-Rohsenow<sup>(20)</sup> Jens and Lottes<sup>(15)</sup> and Thom<sup>(15)</sup>. It is anticipated, based on review of the formulation of the correlations, that the Bergles-Rohsenow correlation predicts the earliest onset of subcooled boiling.



Figure 27 gives a plot of the incipient boiling criteria for the Connecticut Yankee case, assuming that the inlet flow distribution is obtained by using the pressure gradient option in COBRA III C. The results show that subcooled boiling may occur in two spots located on fuel rods No. 3 and 4 at 96.5 in. from the core inlet according to Bergles-Rohsenow. It should be noticed that Westinghouse uses the THOM correlation (21) to predict the onset of subcooled boiling. According to this correlation, no subcooled boiling occurs in the Connecticut Yankee reactor as it can be seen in Fig. 27. Therefore the assumption of very little subcooled voids in the core seems valid.

Furthermore the equilibrium exit quality in each flow region corroborates this conclusion, Fig. 28 gives the assembly outlet distribution of the steam quality, and the highest equilibrium quality is -0.088 in the hot channel.

The comparison between the measured temperature rise of the coolant through a given channel and the expected rise obtained from COBRA III C might also give an indication on the validity of the model. To do this comparison, the measured temperature and the associated uncertainties

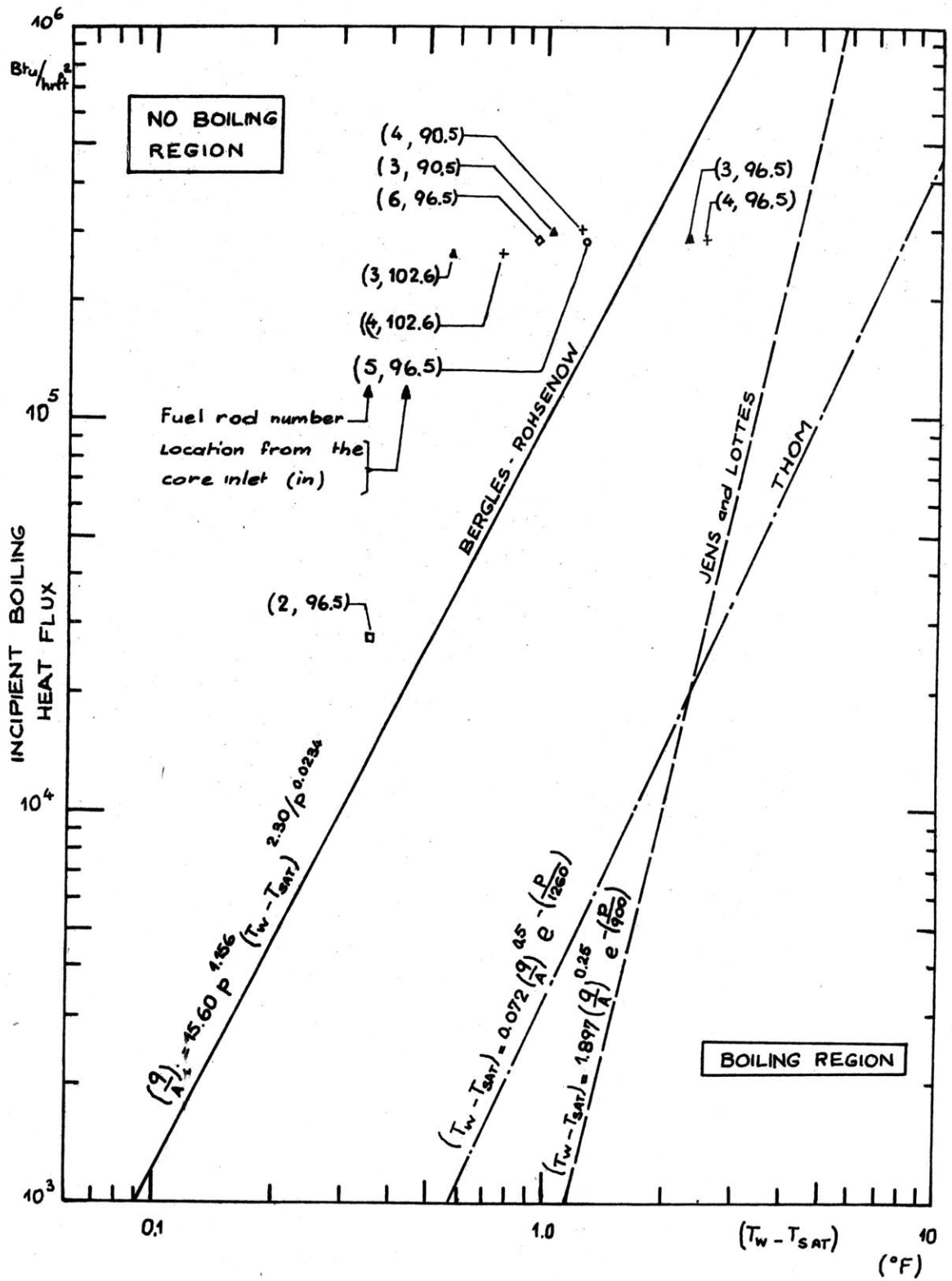


Fig. 27 Incipient boiling criteria applied to the CV case.

	15	14	13	12	11	10	9	8	
R							562.18 564.83 -.1552	565.97 569.83 -.1477	1 2 3 4
					<u>Hottest assembly= N 11</u>				
P					564.61 568.04 -.1504	579.05 587.39 -.1215	588.63 600.48 -.1019	571.88 577.64 -.1360	
N					567.52 571.86 -.1447	591.75 604.89 -.0953	574.88 581.70 -.1300	579.12 587.47 -.1213	579.32 587.75 -.1209
M					581.37 590.56 -.1167	587.66 599.10 -.1039	586.53 597.56 -.1063	586.48 597.49 -.1064	574.64 581.38 -.1305
L					575.73 582.86 -.1282	576.89 584.43 -.1259	577.55 585.33 -.1245	582.63 592.28 -.1141	
K						583.60 593.59 -.1122	584.33 594.58 -.1107	570.30 575.55 -.1392	
J							574.46 581.13 -.1308	579.43 587.90 -.1207	
H								567.90 572.36 -.1439	

- 1: Assembly outlet temperature (from COBRA III C) (°F)
- 2: Assembly outlet enthalpy (Btu/lb<sub>m</sub>)
- 3: Assembly exit quality
- 4: -

595.09 609.63 -.0882	591.68 604.80 -.0954
591.87 605.06 -.0950	591.28 604.22 -.0963

Fig. 28 Coolant quality distribution at the assembly outlet.

Hot subchannels

must be obtained as discussed in 2.3.3. The study developed for the San Onofre Reactor <sup>(9)</sup> uses:

$$t_{\text{corrected}} = t_{\text{measured}} - 0.5 \pm 3.62 \text{ (}^\circ\text{F)} \quad (4.9)$$

This relation is based on the assumption of ref. (9) that an error of  $\pm 3.0$   $^\circ\text{F}$  is due to the imperfect flow mixing or due to the fact that the hot junction location is not in a plane where the coolant temperature is uniform. The hot junction of the thermocouple is located 7 inches above the top of the fuel rods. As it is shown on Fig. 29, the top part of the fuel assembly is fitted with a kind of channel constituting a closed geometry which limits the cross flow exchange with the neighboring fuel assemblies. The only process which takes place in the coolant when it leaves the top of the fuel rods, is thermal mixing. How good is this thermal mixing, is a difficult question to answer.

In a very conservative assumption we may admit that the temperature profile of the coolant leaving the top of the fuel rods is the same when the coolant crosses the plane where the hot junction of the thermocouple is located.

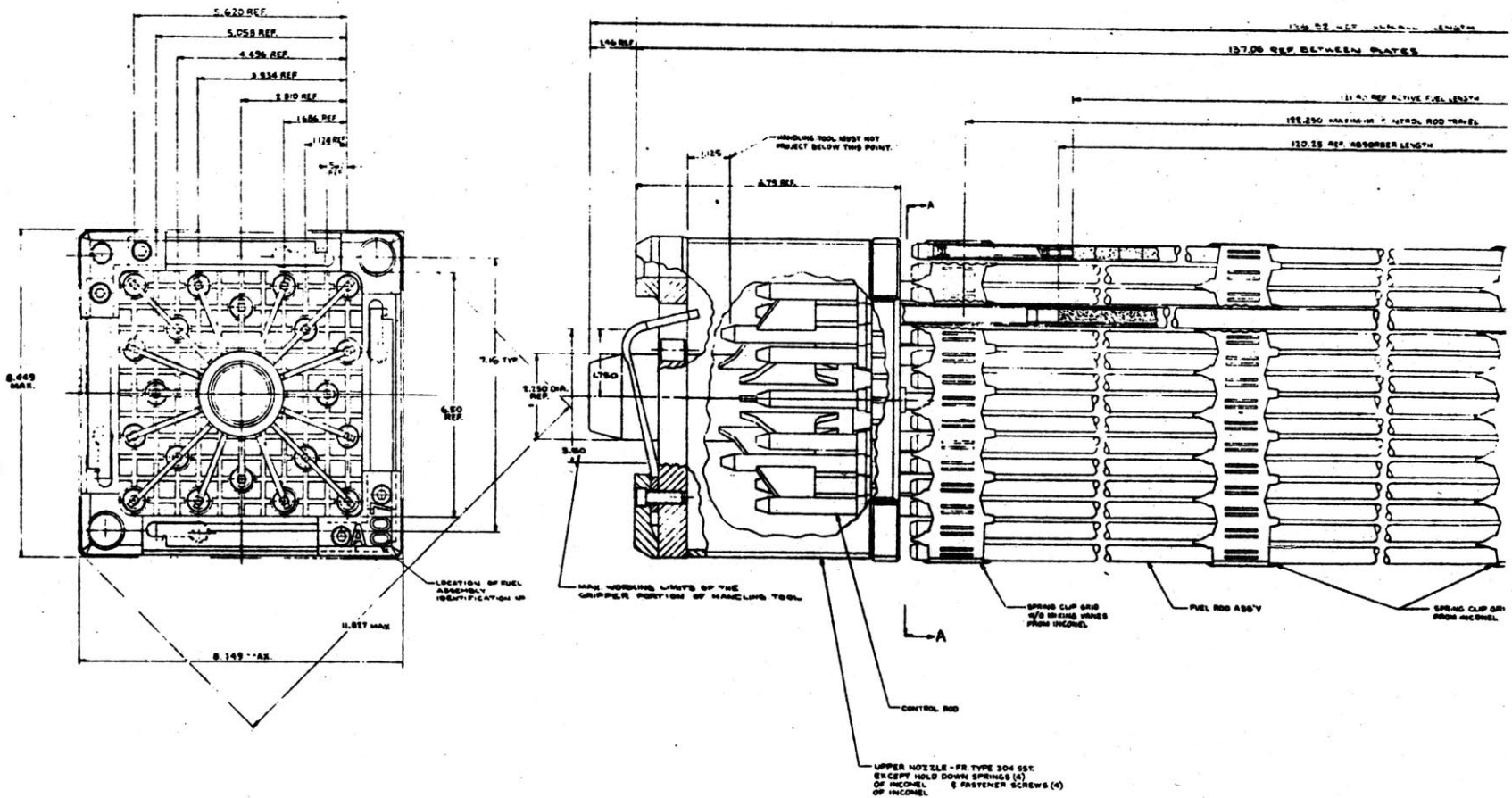


Fig. 29a Fuel assembly (upper part).

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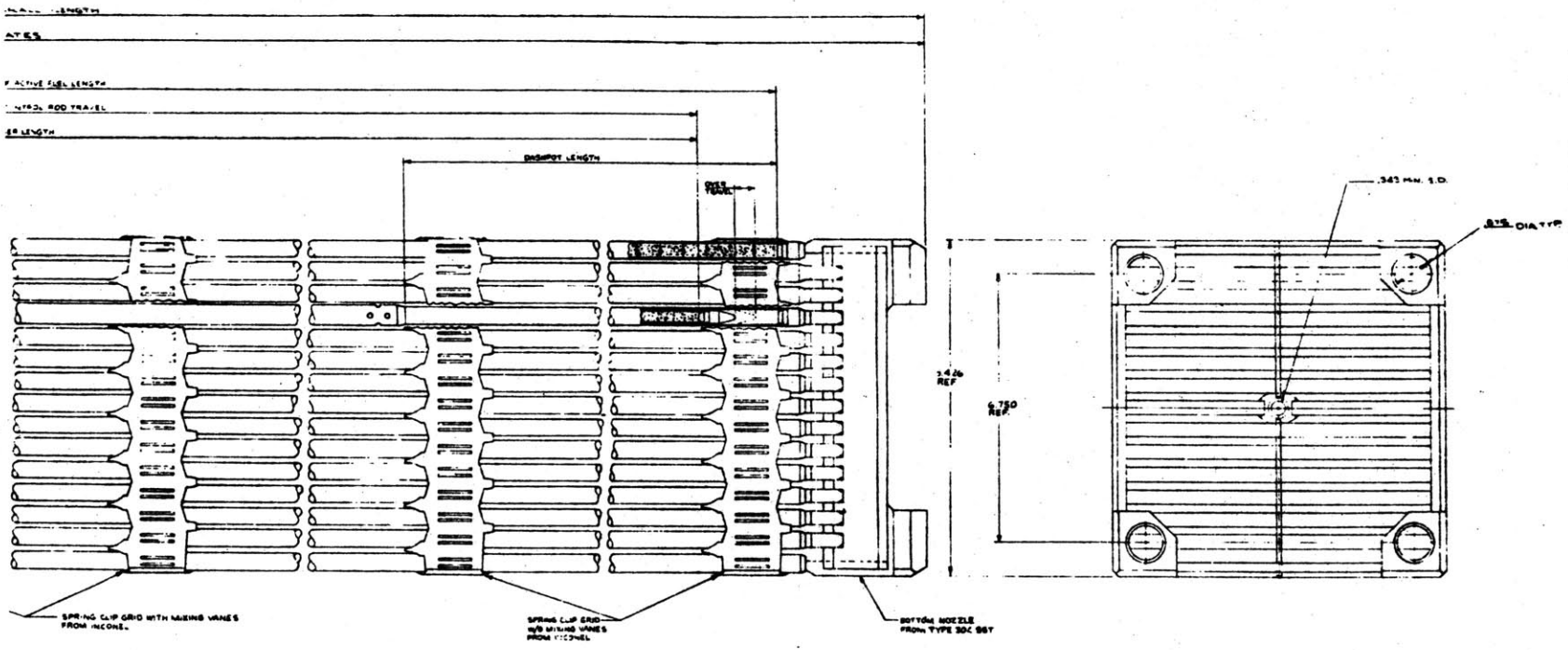


Fig. 29b Fuel assembly (lower part).

As an example COBRA III C has been used to treat the case of the hot assembly and obtain the temperature profile of the coolant at the top of the fuel rods. Figure 30 gives the power distribution used in COBRA III C, and Fig. 31 gives the temperature distribution of the coolant at the top of the fuel rods.

Figure 29 shows that the top of the fuel assembly is engineered with a square opening of 6.50 x 6.50 inches. Therefore the coolant in the peripheral channels is diverted toward the bundle center altering the radial coolant temperature distribution. Figure 31 presents the calculated temperature distribution at the core exit before the flow contraction. It is very difficult to estimate the actual radial coolant temperature profile as a function of axial position. It can be said that the coolant temperature may vary from 595.26°F down to 582.16°F at least. Since the hot assembly in this case is not instrumented with an outlet thermocouple it is difficult to see how exactly the measured temperature compares with the predicted temperature profile.

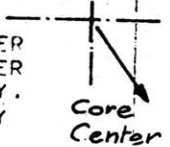
Thus there is not a good method for evaluation of the thermal mixing in a duct when temperature streaming exists at the duct inlet. One might suggest a possible

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Core  
edge

.746	.807	.842	.900	.937	.973	.994	1.010	1.036	1.058	1.063	1.068	1.071	1.053	1.029
.814	.899	.979	1.001	1.041	1.097	1.097	1.091	1.138	1.179	1.159	1.159	1.175	1.122	1.057
.876	.984	0.000	1.107	1.153	0.000	1.228	1.237	1.267	0.000	1.264	1.253	0.000	1.186	1.085
.922	1.017	1.115	1.173	1.237	1.263	1.272	0.000	1.306	1.332	1.337	1.302	1.249	1.185	1.098
.967	1.065	1.171	1.246	0.000	1.247	1.222	1.267	1.250	1.306	0.000	1.350	1.302	1.206	1.114
1.012	1.131	0.000	1.283	1.258	1.211	1.182	1.195	1.205	1.258	1.330	1.379	0.000	1.251	1.132
1.061	1.180	1.266	1.303	1.243	1.193	1.202	1.235	1.221	1.231	1.302	1.382	1.359	1.235	1.135
1.086	1.149	1.286	0.000	1.301	1.216	1.245	0.000	1.260	1.247	1.350	0.000	1.359	1.216	1.138
1.101	1.091	1.329	1.362	1.295	1.239	1.243	1.272	1.256	1.264	1.334	1.414	1.388	1.260	1.156
1.113	1.254	0.000	1.401	1.367	1.307	1.268	1.274	1.278	1.329	1.399	1.444	0.000	1.301	1.173
1.147	1.246	1.349	1.420	0.000	1.397	1.357	1.396	1.366	1.416	0.000	1.454	1.386	1.278	1.175
1.160	1.254	1.351	1.396	1.450	1.464	1.457	0.000	1.465	1.480	1.472	1.423	1.380	1.280	1.180
1.172	1.263	0.000	1.377	1.405	0.000	1.450	1.439	1.457	0.000	1.424	1.599	0.000	1.304	1.185
1.181	1.286	1.384	1.366	1.319	1.362	1.336	1.307	1.342	1.372	1.334	1.319	1.325	1.254	1.172
1.182	1.177	1.209	1.223	1.237	1.252	1.250	1.245	1.254	1.251	1.250	1.230	1.227	1.194	1.155

MAXIMUM FUEL ROD POWER IS 1.480  
 AVERAGE POWER IN ASSEMBLY 1.112 WITH WATER  
 MAXIMUM ROD/AVERAGE POWER 1.331 WITH WATER  
 AVERAGE POWER IN ASSEMBLY 1.227 FUEL ONLY.  
 MAXIMUM ROD/AVERAGE POWER 1.206 FUEL ONLY



EDIT OF ASSEMBLY NUMBER 8  
 ASSEMBLY LOCATION COLUMNS 71 TO 87, ROWS 39 TO 55, PLANES 0 TO 1  
 ALL OF THIS ASSEMBLY IS IN P00  
 NUMBER OF FUEL RODS ALONG COLUMNS 15 AND ROWS 15

FUEL ROD POWERS FOR ASSEMBLY 8 FROM PLANE 0 TO 1

Fig. 30 Power Distribution in the hottest fuel assembly (W 11).



Core edge

568.94	572.46	576.07	578.72	579.69	581.14	582.47	583.91	584.42	585.06	585.70	585.07	583.89	581.76
572.78	574.29	578.21	582.42	582.18	583.87	586.57	588.06	586.33	587.35	589.32	586.64	585.20	584.39
576.22	578.71	582.16	586.03	586.15	587.66	587.94	589.39	590.26	590.71	592.37	590.55	587.65	586.21
579.30	583.26	586.93	586.96	588.36	590.99	589.77	591.10	593.47	592.05	593.55	593.63	591.02	587.77
581.23	583.48	587.17	589.16	589.43	591.54	591.61	592.61	593.33	593.38	593.71	592.72	589.98	588.26
583.26	585.75	589.08	592.13	592.16	591.59	591.23	591.96	594.10	594.80	594.16	593.59	590.92	588.93
584.93	588.77	589.73	591.09	592.57	591.83	589.19	590.79	593.41	594.46	594.31	593.71	593.23	589.59
587.20	591.08	592.10	593.12	592.74	592.50	591.88	592.17	594.47	594.07	594.52	594.88	594.22	590.42
588.11	590.20	593.37	594.34	589.21	591.72	594.94	594.28	594.57	594.50	594.07	594.64	592.77	594.68
589.27	591.34	594.43	594.93	591.55	594.33	594.22	594.37	594.57	594.84	594.56	594.22	593.26	591.18
590.40	593.91	594.78	594.30	594.64	594.83	594.36	594.52	595.26	592.43	595.00	594.37	594.49	591.82
590.23	591.58	594.33	594.67	594.70	594.77	594.70	594.46	591.62	591.19	594.90	594.29	592.80	591.28
589.48	589.96	593.32	594.65	594.30	594.88	595.01	594.75	594.77	594.44	595.05	594.18	592.09	590.28
587.41	590.62	592.42	593.89	594.21	594.61	595.00	595.01	594.76	594.59	594.64	593.33	591.56	588.78

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Core center



Fig. 31 Temperature Distribution at the top of fuel assembly N 11. (BOC)

solution, using COBRA III C for an assembly equipped with a control rod cluster, in which case a possible set of flow regions could be defined above the top of the fuel rods. But the study would be less detailed in this case, since one flow region would have to correspond to several subchannels. This type of analysis would still only lead to average results.

Figure 32 is a plot of the measured temperature rise of the coolant versus the predicted temperature rise. The uncertainty associated with the temperature measurement is also plotted (Eq. 4.9). The least square fit analysis of the data on Fig. 32 leads to:

$$t_{\text{corrected}} = 0.854 t_{\text{measured}} + 7.43 \pm 4.27 \text{ (}^\circ\text{F)}, \quad (4.10)$$

It is important to recognize that the power distribution in the fuel assembly is time dependent for a given assembly and at a given time varies from assembly to assembly. Therefore the temperature profiles that may be obtained from the different power distributions would considerably vary.

Measured temperature  
rise (Thermocouples)

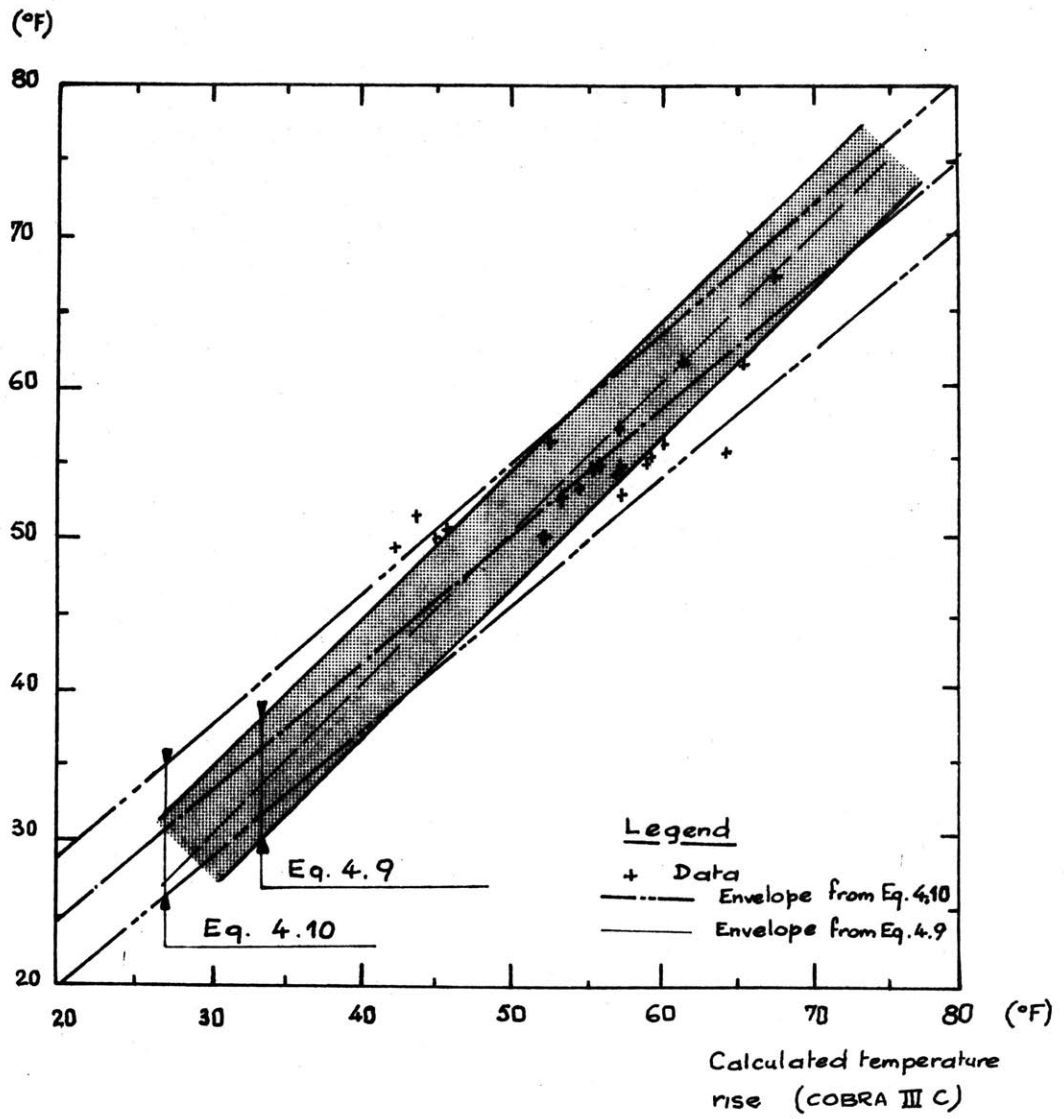


Fig. 32 Measured temperature rises versus calculated temperature rises.

It may be concluded that the treatment of the core octant by COBRA III C is valid and gives satisfactory information. Furthermore, it should be mentioned that the actual MDNBR, the maximum clad surface temperature, the maximum fuel centerline temperature are within the limits of the PSAR <sup>(2)</sup> as it can be seen below:

	Calculated value (from COBRA III C) (for a two sigma confidence level)	Reference (from PSAR)
MDNBR	3.891 ± 0.243	2.03
Max clad surface temp. (°F)	637.1 ± 5.1	652
Max fuel centerline temp (°F)	2,724.9 ± 109.9	3,920

These extra margins for the steady state operation of the Connecticut Yankee Reactor can be explained by the fact that the core is slightly subcooled, the actual average temperature of the coolant in the core is about 550°F instead of the 575°F design value <sup>(2)</sup>. This conservative operation is very favorable for the fuel and clad operation since it tends to limit the number of clad failures.

The COBRA results indicate also that the cross flow exchange has very little effect on the assembly exit conditions, and therefore will not be possible to obtain

cross flow exchange information between assemblies from the assembly exit thermocouples readings. Furthermore, the inlet flow distribution at the bottom of the core does not greatly influence the assembly exit conditions, is due to the fact that the core is slightly subcooled with very little subcooled boiling taking place.

## CHAPTER 5

### FINAL ANALYSIS OF THE CONNECTICUT YANKEE DATA

#### 5.1 Introduction

From the results developed in Chapters 3 and 4 a method of evaluation of the uncertainty associated with the peaking factors can be established.

The flow calculations done with COBRA III C give the results for the assembly exit conditions that have been shown to be independent of several parameters or inlet flow distribution used for the computation. This indicates that the flow pattern is relatively stable and the core is operated under highly subcooled conditions. Also it is found to be difficult to predict the cross flow pattern from the information given by the thermocouples and the power distribution.

In this chapter a new version of FLOEA 1 and 2 is given which allows the use of uncertainties associated with each measurement that may vary from assembly to assembly.

#### 5.2 Determination of the Uncertainty of the Peaking Factors

From the results of the sensitivity analysis done on the code "INCORE" (see Chapter 3), the uncertainties associated with:

- the same type of information (for example all the flux detector readings used in the calculation of the peaking factors in a given assembly) are combined according to Eq. 28 of Ref. 22:

$$p_{\bar{x}} = \frac{1}{\sqrt{\sum_{n=1}^N \left( \frac{1}{p_n \bar{x}} \right)^2}},$$

- where:
- $p_{\bar{x}}$  = the probable error on  $\bar{x}$
  - $p_n \bar{x}$  = the probable error on  $\bar{x}_n$
  - $N$  = the number of measurements on  $x$  used to compute  $\bar{x}$ ,

- the different informations used to compute the peaking factors in a given assembly are combined statistically, since these informations are independent from each other.

As an example, taking the case of a specific collection of data at BOC of Core III (run 89):

- the code "INCORE" gives:

- $\text{Maxi } F_{\Delta H}^N = 1.5026$  for the hottest fuel rod in N 11,

- $\text{Maxi } F_q^N = 1.8584$  for the hottest fuel rod in N 11,
- the peaking factors for the hottest fuel rod in N 11 are calculated from the information given by three flux thimbles P 10, M 10, M 12.

For one sigma confidence level it may be established:

- Radial distance of the hottest fuel rod: 83.01 pitches  
in N 11 or 46.73 inches.
- For 1% increase in the flux detector readings:
  - uncertainty due to P 10 (curve B Fig. 7b) = 0.00325
  - uncertainty due to M 10 (curve B Fig. 7b) = 0.00325
  - uncertainty due to M 12 (curve B Fig. 7b) = 0.00325
  - uncertainty for the hottest fuel rod in  
N 11 due to flux detectors = 0.001876.
- For 4% decrease in the flux thimble prediction:
  - uncertainty due to P 10 (curve B Fig. 9b) = 0.01320
  - uncertainty due to M 10 (curve B Fig. 9b) = 0.01320
  - uncertainty due to M 12 (curve B Fig. 9b) = 0.01320
  - uncertainty for the hottest fuel rod in  
N 11 due to flux thimble prediction uncertainties  
= 0.007621
- For 4% increase in the power prediction:
  - uncertainty due to P 10 (see 3.4.3) = 0.04000
  - uncertainty due to M 10 (see 3.4.3) = 0.04000



- uncertainty due to M 12 (see 3.4.3) = 0.04000
- uncertainty due to the power prediction  
uncertainties = 0.023094

- For 1 sigma confidence level the relative uncertainty in N 11 is given by:

- uncertainty due to flux detector readings = 0.001876
- uncertainty due to flux thimble prediction = 0.007621
- uncertainty due to power prediction = 0.023094
- relative uncertainty for the hottest fuel rod  
in N 11 = 0.024391

Absolute uncertainty on  $F_{\Delta H}^N$  for two sigma confidence level:

$$0.02439 \times 2 \times 1.5026 = 0.0733.$$

The maximum  $F_{\Delta H}^N$  for a two sigma confidence level is given by:

$$F_{\Delta H}^N = 1.5026 \pm 0.0733.$$

Similarly the uncertainty on  $F_q^N$  for two sigma confidence level is given by the statistical combination of:

- relative uncertainty associated with  $F_{\Delta H}^N$ ,
- relative uncertainty associated with the local peaking factor  $F_z$  (taken equal to the uncertainty due to the flux detector reading).

This combination leads to:

$$F_q^N = 1.8584 \pm 0.0980 .$$

$$\text{Since } F_q^E = 1.04 \text{ (2)}$$

$$F_q = 1.04 \times 1.8584 \pm 0.0980 = 1.9327 \pm 0.1019 .$$

The maximum linear heat generation rate is then:

$$\text{MLHGR} = F_q \times \frac{\text{kW}}{\text{MW}} \times \frac{1}{\text{total heated length(ft)}}$$

x thermal power (MWt)

$$= (1.9327 \pm 0.1019) \times 0.003096 \times 1825$$

$$= 10.920 \pm 0.576 \text{ kW/ft} .$$

This value is related to a two sigma confidence level.

The thermal power is taken as the rated power in a conservative manner even if the real power was below this value while the flux map was recorded. If the thermal power is taken as 1813.5 MWth power at which the data were

collected, the MLGHR is then:  $10.851 \pm 0.529$  kW/ft.

This gives a method for evaluating the uncertainty associated with the peaking factors. This same method may also be used to evaluate the uncertainties in the power distribution by taking each fuel assembly individually. This method shows that the uncertainty becomes smaller when the number of thimbles used for the calculation of the peaking factor in a given assembly, is increased.

The uncertainty evaluation is based on the assumption that the uncertainty due to the power prediction is estimated to be  $\pm 4\%$  and  $\pm 4\%$  for the flux thimble prediction, for one sigma confidence level. This should be confirmed by further work, by doing a sensitivity analysis on the main parameters of the PDQ code.

### 5.3 Second Sensitivity Analysis on the Effective Flow Factors

Using the method developed in 5.2, the uncertainty on the power prediction can be evaluated for each assembly. The uncertainty on the coolant assembly exit temperature has been evaluated in a global manner by Eq. 4.10, however one may provide in the future a more detailed analysis of the temperature uncertainty.

The two versions of the code developed in Chapter 2 FLOFA 1 and 2, have been remodeled to allow the use of

the uncertainties on the power distribution and the exit temperature of the coolant for each assembly. This differs from the versions in Chapter 2, where only a unique value of the accuracy for each quantity was used for all the assemblies.

FLOFA 3 and FLOFA 4 are the new versions of the codes used for the evaluation of the uncertainties in the effective flow factors. They give very similar information to the one given by the original versions. (See Appendix B for the codes listings and sample input and output.)

The results for the two types of calculations are compared with the original versions on Fig. 33 and 34. The remarks and the conclusions remain unchanged from those obtained in Chapter 2. However the main interest with the new versions of FLOFA is constituted by the fact that individual inaccuracies can be selected.

#### 5.4 Other Remarks on the Connecticut Yankee Data

##### 5.4.1 Core Symmetry

The dissymmetric effect which appears in the power distribution is due to the fact that the only symmetry which can be maintained in the core is a quadrant symmetry. This is due to the fact that the changes in isotopic compositions for fuel elements in geometrical symmetrical positions in the core, are not the same in these fuel

	15	14	13	12	11	10	9	8	
R							-	0.8081	1
							-	5.6515	2
							-	5.8334	3
							-	4.001	4
<b>Hottest assembly= N 11</b>									
P					0.8086	1.0254	0.9859	-	
					5.8389	5.5036	4.7698	-	
					7.0651	6.8914	4.6098	-	
					5.506	5.539	3.157	-	
N				0.8563	-	0.9001	1.0160	1.0645	
				5.7859	-	5.3063	5.4520	5.6114	
				6.5419	-	4.9418	4.6869	5.1995	
				4.863	-	3.029	2.360	3.057	
M			-	0.9515	1.0387	1.1291	1.0165	-	
			-	5.0493	4.9941	5.3534	4.9834	-	
			-	4.7828	4.2686	4.8775	4.2714	-	
			-	3.095	2.309	2.859	2.331	-	
L		0.7304	1.0716	1.0008	0.9728	0.9936	0.9817	1.0443	
		5.5721	4.9410	4.8649	5.5490	5.5337	5.4376	5.5879	
		6.4745	4.6939	4.1988	4.6660	4.7446	4.6605	5.5879	
		4.955	3.087	<b>2.382</b>	2.143	2.336	2.332	4.010	
K		1.0340	0.9488	1.2321	0.9933	1.1431	-	-	
		5.6760	5.5337	5.6842	5.5036	5.5956	-	-	
		6.3849	5.1003	4.8757	4.7144	4.7868	-	-	
		4.743	2.993	2.341	2.327	2.314	-	-	
J	0.8971	1.0453	-	1.0434	-	1.0460	1.0041	1.0336	
	6.3659	4.8551	-	5.0050	-	5.1422	5.7859	5.4813	
	7.5710	4.3514	-	4.2899	-	4.4078	4.9486	5.7327	
	5.745	2.655	-	2.331	-	2.332	2.311	4.029	
H	0.9340	1.0319	1.2905	0.9864	1.0402	0.9639	1.0121	0.9242	
	6.1476	5.7510	5.7514	5.4887	5.1542	5.9587	5.3741	6.0560	
	7.4375	5.3184	5.2328	5.0049	4.7066	5.3553	4.8918	6.1244	
	5.745	3.059	2.920	2.891	2.841	2.836	2.855	4.002	

- 1: Effective flow factor: EFF
- 2: Relative uncertainty on EFF (%), assuming: relative power uncertainty=2.75%, outlet temp. uncertainty= 2.5°F, inlet temp. uncent.=0.1°F
- 3: Relative uncertainty on EFF (%), assuming: relative power uncertainty= value given in 4:, outlet temp. uncertainty= 2.14 °F, inlet temp. uncertainty= 0.1°F
- 4: Relative power uncertainty (%) used to compute 3:

**Fig. 33** Comparison of the uncertainties associated with the effective flow factors. Heat capacity of the coolant independent of the temperature.

	15	14	13	12	11	10	9	8		
R							-	0.8110	1	
							-	5.9173	2	
							-	6.0232	3	
							-	4.001	4	
<u>Hottest assembly</u> - N 11										
P	All the uncertainties are related to a one sigma confidence level.				0.8138	1.0268	0.9721	-		
					6.1048	5.7699	5.0507	-		
					7.2277	7.0490	4.8239	-		
					5.506	5.539	3.157	-		
N				0.8611	-	0.8986	1.0165	1.0677		
				6.0517	-	5.5738	5.7186	5.8773		
				6.7156	-	5.1529	4.9139	5.4102		
				4.863	-	3.029	2.360	3.057		
M										
L										
K										
J										
H										

1: Effective flow factor: EFF

2: Relative uncertainty on EFF (%), assuming: relative power uncertainty=2.75%, outlet temp. uncertainty=2.5°F, inlet temp. uncert.=0.1°F

3: Relative uncertainty on EFF (%), assuming: relative power uncertainty= value given in 4:, outlet temp. uncertainty=2.14°F, inlet temp. uncertainty=0.1°F

4: Relative power uncertainty (%) used to compute 3:

Fig. 34 Comparison of the uncertainties associated with the effective flow factors. Heat capacity of the coolant temperature dependent.

elements. In fact the coolant temperature at the core inlet is not uniform, and the corresponding variation is about  $\pm 2.5$  °F, as it can be seen on data collected at the plant.

Furthermore, as it is shown in Fig. 35 the relative disposition of the inlet nozzles and outlet nozzles tends to favor asymmetry in the inlet temperature distribution and therefore in the power distribution. If the inlet nozzles were located at 90° from each other, instead of 45° and 135°, the inlet temperature of the coolant would probably be more symmetric.

#### 5.4.2 Effective Flow Factors Variations

An arbitrary increase of the power in assembly N 9 by 10% has been done to compare the variations of:

- the flow distribution at the assembly exit, using COBRA III C,
- the coolant temperature distribution at the assembly exit,
- the effective flow factor distribution, assuming that the measured coolant temperature rise in assembly N 9 stays constant,

between the "reference case" (power in N 9 unchanged) and a "new core" (power in N 9 increased by 10%).

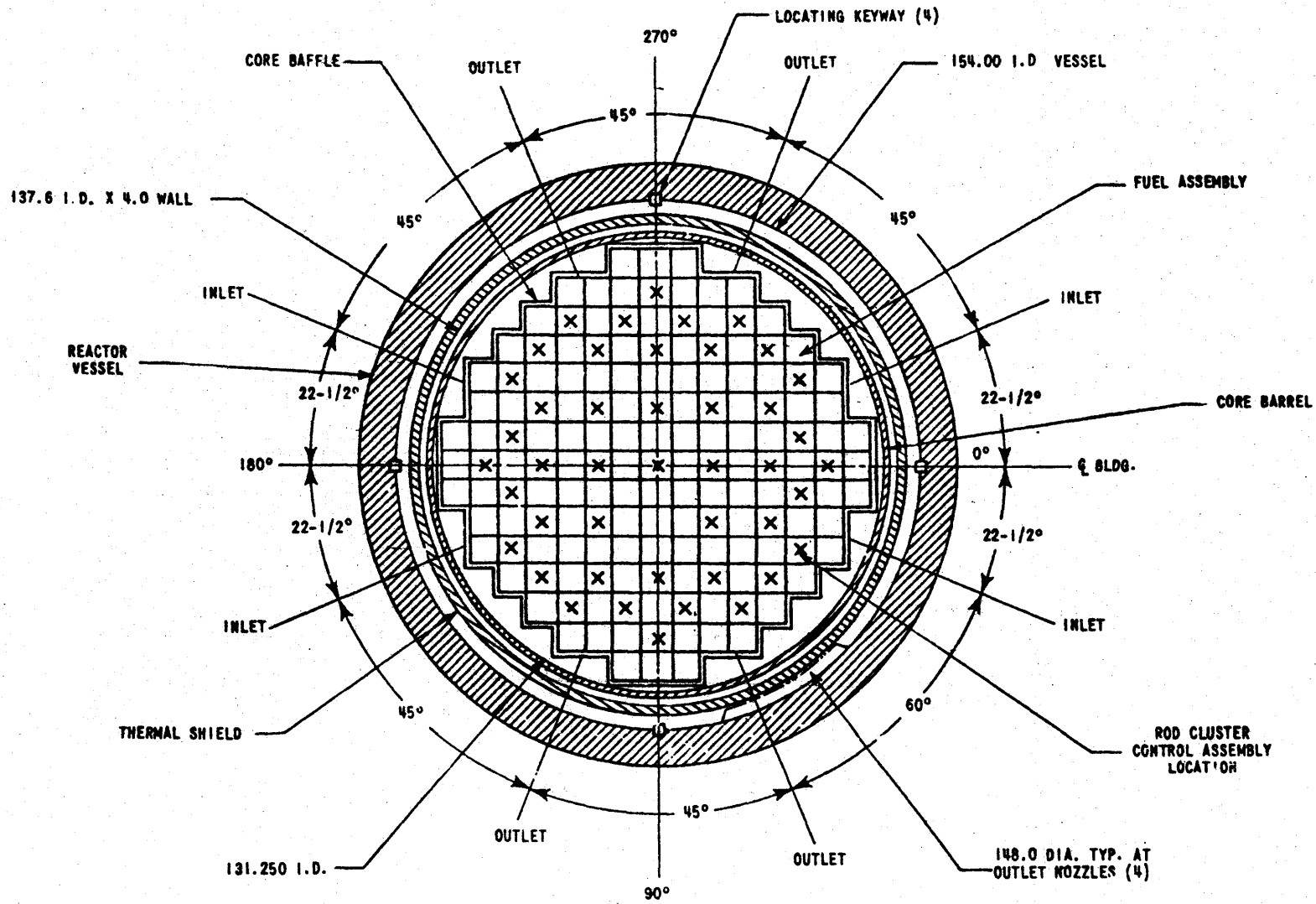


Fig. 35 REACTOR CORE CROSS SECTION



coolant for the assemblies on the edge of the core is lower than the measured temperature. But the computation of the temperature is based on the power distribution obtained from INCORE.

It is noticeable that the calculated value of the power for the assemblies on the edge of the core is, in most of the cases, greater than the predicted value obtained from the PDQ calculation. Combining this remark with the fact that the COBRA calculations would lead to higher coolant temperatures at the exit of the peripheral assemblies if higher power distribution were used, would seem to indicate that the power distribution of the assemblies at the edge of the core may be underestimated. There is no absolute evidence to support this argument, however it is also difficult to explain the low values of the effective flow factors. More than a flow distribution, the effective flow factors seems to give an indication of the quality of the match between the core physics analysis and the thermal hydraulic analysis. An effective flow factor of one would tell that both analysis agree with each other.

#### 5.4.3 Round Off Errors

Since all the information is treated by the computer, one may worry about the round off problem. The problem is

When the power in N 9 is increased by 10%:

- Fig. 36 shows that the coolant temperature distribution at the assembly exit is unchanged, except in assembly N 9, Table 6 indicates a relative increase of 9.47% for the calculated coolant temperature rise,

- Fig. 37 shows that the normalized flow distribution at the assembly exit is increased by a constant quantity = 0.0002 in each assembly, except in N 9 where it is reduced by a constant quantity = 0.0035,

- Fig. 37 indicates a decrease of the effective flow factor by about 0.003, except in N 9 where it is increased by 0.0994.

It is important to recognize that, the effective flow factor and the coolant flow distribution at the assembly exit varies in opposite directions for a local variation of power (as in this case in one assembly).

The values of the effective flow factors for the assembly on the edge of the core are always lower than the values for assembly well within the core. This would mean that either the estimated coolant temperature rise is too large or the calculated relative power is too small for the fuel assemblies on the edge of the core. The study developed in Chapter 4, using COBRA III C seems to indicate that the calculated exit temperature of the

	15	14	13	12	11	10	9	8	
R							562.20	565.75	1
							562.19	565.75	2
							-	573.8	3
								0.769	4
<b>Hottest assembly= N 11</b>									
P					564.63	579.03	588.67	571.91	
					564.62	579.05	588.65	571.91	
					571.6	575.7	588.2	-	
					0.737	1.012	1.201		
N				567.51	591.77	574.89	584.49	579.37	
				567.52	591.76	574.89	579.11	579.35	
				572.2	-	578.5	576.4	574.3	
				0.790		0.935	1.016	1.023	
M					581.40	587.66	586.59	586.53	574.66
					581.39	587.66	586.56	586.50	574.65
			-		582.7	583.7	577.8	583.9	-
					1.062	1.178	1.158	1.157	
L						575.71	576.84	577.66	582.68
						575.72	576.88	577.53	582.63
		574.8	584.7	586.2	575.1	575.3	576.6	578.7	
		0.709	1.236	1.182	0.949	0.973	0.985	1.068	
K						583.68	584.38	570.51	
						583.63	584.37	570.50	
		573.5	575.3	573.4	575.7	574.5	-	-	
		0.978	0.929	1.163	0.980	1.103			
J							574.36	579.30	
							574.38	579.32	
	566.4	586.4	-	583.5	-	580.8	572.2	576.0	
	0.731	1.238		1.180		1.137	0.926	1.026	
H								567.86	
								567.80	
	568.4	572.5	572.6	575.9	580.9	570.3	577.5	569.3	
	0.796	0.957	1.199	0.977	1.126	0.855	1.032	0.803	

- 1: Coolant temperature at the assembly outlet  
( power in N 9 increased by 10 % )
- 2: Coolant temperature at the assembly outlet  
( reference case )
- 3: Coolant temperature at the assembly outlet  
( measured value by outlet thermocouple )
- 4: Relative power of the assembly

595.09	591.66
595.10	591.69
-	-
591.75	591.21
591.87	591.28
-	-

**Fig. 36** Coolant temperature distribution at the assembly exit. Power increase in N 9 case.

**Hot subchannels**

	15	14	13	12	11	10	9	8	
R							1.0063	1.0058	1
							1.0065	1.0060	2
							-	0.8081	3
							-	0.8060	4
							<b>Hottest assembly- N 11</b>		
P					1.0051	0.9974	0.9927	1.0044	
					1.0053	0.9976	0.9929	1.0046	
					0.8086	1.0254	0.9859	-	
					0.8069	1.0229	0.9829	-	
N				1.0034	0.9906	1.0029	1.0000	0.9997	
				1.0036	0.9908	1.0031	0.9965	0.9999	
				0.8562	-	0.9001	1.0160	1.0645	
				0.8534	-	0.8980	1.1154	1.0619	
M					0.9980	0.9940	0.9952	1.0066	
					0.9982	0.9942	0.9954	1.0068	
					-	0.9515	1.0387	-	
					-	0.9490	1.0355	-	
L						1.0028	0.9996	1.0024	0.9986
						1.0030	0.9998	1.0026	0.9988
		0.7303	1.0716	1.0008	0.9728	0.9936	0.9817	1.0443	
		0.7289	1.0691	0.9984	0.9701	0.9909	0.9791	1.0412	
K						0.9980	0.9980	1.0076	
						0.9982	0.9982	1.0078	
		1.0340	0.9498	1.2321	0.9933	1.1430	-	-	
		1.0310	0.9461	1.2284	0.9906	1.1405	-	-	
J							1.0050	1.0015	
							1.0052	1.0017	
	0.8971	1.0453	-	1.0434	-	1.0460	1.0041	1.0336	
	0.8947	1.0425	-	1.0407	-	1.0437	1.0016	1.0313	
H								1.0098	
								1.0100	
	0.9340	1.0319	1.2890	0.9864	1.0402	0.9639	1.0121	0.9242	
	0.9320	1.0290	1.2867	0.9838	1.0371	0.9614	1.0091	0.9222	

- 1: Normalized flow distribution at assembly outlet (reference case)
- 2: Normalized flow distribution at assembly outlet (power in N 9 increased by 10 %)
- 3: Effective flow factor ( $C_p$ ) (reference case)
- 4: Effective flow factor ( $C_p$ ) (power in N 9 increased by 10 %)

0.9934	0.9781
0.9936	0.9782
-	-
-	-
0.9784	0.9790
0.9785	0.9792

**Fig. 37** Normalized flow distribution at the assembly exit. Power increase in N 9 case.

**Hot subchannels**

	Reference Case	New Case	Relative Variation
Relative assembly power	1.016	1.118	+ 10 %
Effective flow factor	1.0160	1.1154	+ 9.78 %
Normalized assembly outlet flow	1.0000	0.9965	- 0.35 %
Normalized assembly inlet flow	1.0065	1.0065	
Measured coolant temperature rise	54.1°F	--	
Calculated coolant temperature rise	56.81°F	62.19°F	+ 9.47 %

Table 6 Relative Variation of the Effective Flow Factor and Normalized Assembly Outlet Flow in N 9

not very difficult to treat but rather long. It may be recognized that most of the results in the computations are presented according to a normalized distribution which tends to limit the round off error problem. Varying the last figure of the temperature rise or of the power prediction in the calculation of the effective flow factor influenced the values of the effective flow factors by less than a percent, because of the normalization of the results. As far as the uncertainty problem is concerned, the round off problem is of a second order as compared to the other sources of inaccuracy.

## CHAPTER 6

### CONCLUSIONS AND RECOMMENDATIONS FOR FUTURE WORK

The study which has been developed here can be divided in different areas:

- sensitivity studies on the codes INCORE and COBRA III C,
- uncertainties evaluation of
  - temperature measurement
  - peaking factors (assembly power distribution)
  - effective flow factors,
- modification of COBRA III C to accommodate the size of the Connecticut Yankee problem,
- analysis of operating data from Connecticut Yankee.

#### 6.1 Sensitivity Studies

##### 6.1.1 Sensitivity Study on the Code "INCORE"

The study has been performed to evaluate the uncertainty associated with:

- peaking factors  $F_{\Delta H}^N$ ,  $F_Q^N$ ,  $F_z$  (results of the INCORE calculation) for assembly averaged values and hot fuel rod

in each assembly from the knowledge of the inputs of the code INCORE:

- flux detector readings (measured values),
  - flux thimble prediction,
  - power distribution prediction
- } obtained from the code  
PDC.

This sensitivity study leads to the following results:

- flux measurements uncertainty (flux detector reading)
  - $F_{\Delta H}^N$  and  $F_Q^N$  are affected, their change behavior is correlated by Fig. 7a and 7b for 1% change in the flux detector reading,
  - $F_Z$  is unaffected,
- flux prediction uncertainty (flux thimble prediction)
  - $F_{\Delta H}^N$  and  $F_Q^N$  are affected, their change behavior is correlated by Fig. 9a and 9b for 1% change in the flux thimble prediction,
  - $F_Z$  is unaffected,
- power distribution prediction
  - $F_{\Delta H}^N$  and  $F_Q^N$  are affected, they undergo 1% change for 1% change in the power prediction,
  - $F_Z$  is unaffected.

These results allow the evaluation of the uncertainty associated with the peaking factors.



### 6.1.2 Sensitivity Study on the Code "COBRA III C"

The study has been done to determine the most adequate value of the parameters to be selected for the calculations. The parameters used in the study are:

- axial node length,
- flow convergence factor,
- S/L parameter defining the control volume,
- turbulent momentum factor,
- cross flow resistance factor,
- type of coolant flow distribution at the core inlet.

The results of this study leads to the conclusions:

- as a general conclusion the coolant conditions (axial flow, temperature, enthalpy) are weak functions of these parameters and do not vary greatly as can be seen in Chapter 4,

- the following values of the parameters provide the best accuracy of the results that can be achieved without any unnecessary increase of the computing time:

axial node length = 6 in,

flow convergence factor = 0.01,

- S/L parameter defining the control volume = 0.25,
- turbulent momentum factor = 0.5,

- cross flow resistance factor = 0.5,
- type of coolant distribution at core inlet  
= equal pressure gradient at core inlet.

For the operation point of view, it may be concluded that because of the insensitivity of the coolant conditions at the core exit a cross flow pattern change cannot be directly observed from the outlet thermocouples. However, further work in this area by simulation of flow blockage at the core inlet for one assembly, then for one subchannel, using COBRA III C should be useful and provide a check of the previous conclusion.

## 6.2 Evaluation of Uncertainties

### 6.2.1 Temperature Measurement

Very little data exists now on the uncertainty associated with temperature measurement in a reactor. However by using the results developed for the San Onofre Reactor<sup>(9)</sup>, and by comparing the measured values and calculated values (using "COBRA III C") of the coolant temperatures at the core exit, the uncertainty on the temperature measurement of the coolant at core exit can be evaluated by Eq. 4.10.

$$t_{\text{corrected}} = 0.854 t_{\text{measured}} + 7.43 \pm 4.27 \quad (^\circ\text{F})$$

This uncertainty on the temperature is to be used in the evaluation of the uncertainty associated with the effective flow factor.

### 6.2.2 Peaking Factors

By using the results of the sensitivity analysis done on the code "INCORE", the uncertainty associated with the peaking factors is calculated according to the procedure described in Chapter 5. As an example, using data taken on the Connecticut Yankee Reactor at BOC of Core III (run 89), for the hottest assembly N 11 it has been found:

$$F_{\Delta H}^N = 1.5026 \pm 0.0733$$

$$F_q^N = 1.8584 \pm 0.0980$$

$$F_q = 1.9327 \pm 0.1019$$

for a two sigma confidence level, or 4.87% and 5.27% of relative uncertainty on  $F_{\Delta H}^N$  and  $F_q$  respectively.

The evaluation of these uncertainties associated with the peaking factors, allows the evaluation of the uncertainty associated with the maximum linear generation, in this particular case it has been found:

$$MLHGR = 10.920 \pm 0.576 \text{ kW/ft}$$

for a two sigma confidence level.

The evaluation of the uncertainty associated with each peaking factor is based on the assumption that the uncertainty associated with the flux thimble prediction and the power distribution prediction is 4% for one sigma confidence level. Further work on the code PDQ should be done to evaluate the uncertainty associated with flux thimble and power distribution predictions, due to the uncertainty associated with the fuel enrichment or other quantities (such as mesh spacing) used as inputs in the code "PDQ". Further work can be done also to check the time independence of the curves in Fig. 7 and 9 from one core to another.

### 6.2.3 Effective Flow Factors

The uncertainty associated with the effective flow factors has been evaluated from the knowledge of the uncertainties associated with temperature measurements and power distribution calculations.

For one sigma confidence an average 6% uncertainty has been found for the effective flow factor. A large fraction (about 70%) is due to the uncertainty on the coolant temperature measurement at the assembly outlet. This uncertainty is rather large compared to the possible variations of the coolant flow distribution from one assembly to another.

### 6.3 Modification of the Code "COBRA III C"

The original version of the code "COBRA III C" was too small to accommodate the size of the Connecticut Yankee problem. The changes have been made on:

- flow channels number increase from 15 to 30,
- flow channels ~~connections~~ number increase from 30 to 47,
- fuel rods number increase from 15 to 35,
- fuel types number increase from 2 to 3,
- axial node number decrease from 60 to 30,
- axial heat flux nodes number increase from 30 to 39.

Appendix C of this work presents a method to handle easily further changes in the code and should be useful for a future user of the code "COBRA III C".

### 6.4 Analysis of Operating Data From Connecticut Yankee

The analysis of the operating data from Connecticut Yankee gave an opportunity to evaluate uncertainties associated with the information obtained from the core instrumentation or quantities derived from the core instrumentation.

The sensitivity study done on the code "COBRA III C", applied to the Connecticut Yankee case shows the weak dependence of the assembly exit conditions of the coolant. This is due to the fact that the core is operated with a fair degree of subcooling. Hence, the actual values of

some critical parameters like DNBR, MLHGR, maximum clad outside temperature, maximum fuel centerline temperature are conservatively within the limits of the technical specifications.

The effective flow factor concept in fact gives more information on the quality of the agreement between the reactor physics analysis and the thermal hydraulic analysis of the core, than on the coolant distribution through the core. A good agreement between reactor physics and thermal hydraulic analysis in a given assembly would lead to an effective flow factor near 1.0 for that assembly. The low values of the effective flow factors for the assemblies located on the core edge, seem to indicate underprediction of the average assembly power. Further work on the power distribution calculation for the peripheral assemblies, using different power predictions should clarify this point.

## APPENDIX A

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## APPENDIX B

The following section contains the codes listings, samples inputs and outputs of the codes used in this work.

```

C      PROGRAM FLOFA I
C*****
C CASE EFFECTIVE FLOW FACTOR DISTRIBUTION
  IMPLICIT REAL*8 (A-H,O-Z)
  REAL *8 LEFT, RIGHT, ASPEC, FSPEC, BLANKS
  REAL*8 LEFTA, RIGHTA, ASPECA, FSPECA, BLANKA
  DIMENSION PESUL1(8,8,4), RESULT2(8,8,5), RESULT3(8,8,8),
  1SIRTIN(8,8), Q(8,8), TOUT(8,8), Y(8,8), X(8,8), SIRTOU(8,8), SPO(8
  2,8), STO(8,8), STI(8,8), SI2Y(8,8), SI2RFL(8,8),
  3SIFLO(8,8,5), FLOFA(8,8,5), SI2FLO(8,8,5), SIPFLO(8,8,5),
  4CONOR(8,8,8), COPOL(8,8,8), COTO1(8,8,8), COTI1(8,8,8), COPO2(8,8,
  58), COTO2(8,8,8), COTI2(8,8,8),
  6SIRPO(10), SITOUT(10), SITIN(10), SUMY(1), FANOR(1), SPOSUM(10),
  7STOSUM(10), STISUM(10), SZYSUM(10), A(10), COLUMN(4),
  8BFORM(10), RUN(3), FORMA(10), COLUMI(8), COLUMK(5), COLUMM(8)
  READ (5,8) RUN
  8  FORMAT(5A8)
  READ (5,9) POWER
  9  FORMAT (A8)
  READ(5,10) NUM, TIN, NUM2
  10 FORMAT(I2,7X,F10.0,4X,I3)
  READ(5,11) LEFTA, RIGHTA, ASPECA, FSPECA, BLANKA
  11 FORMAT(5A8)
  READ (5,12) LEFT,RIGHT, ASPEC, FSPEC, BLANKS
  12 FORMAT(5A8)
  READ (5,13) (COLUMI(I), I=1,8)
  13 FORMAT(8A8)
  READ (5,18) (COLUMK(K), K=1,5)
  18 FORMAT(5A8)
  READ (5,19) (COLUMM(M), M=1,8)
  19 FORMAT(8A8)
  READ (5,5) (COLUMN(N), N=1,4)
  5  FORMAT(4A8)
  DO 14 I=1,8
  DO 14 J=1,8
  TOUT(I,J)=0.0
  Q(I,J)=0.0
  Y(I,J) = 0.0
  X(I,J) =0.0
  SIRTOU(I,J)=0.0
  SIRTIN(I,J)=0.0
  SPO(I,J)=0.0
  STO(I,J)=0.0
  STI(I,J)=0.0
  SI2Y(I,J) =0.0
  14 CONTINUE
  DO 16 IN = 1, NUM2
  READ (5,15) I, J, XQ, XTOUT
  15 FORMAT(2(I2,1X),2(F10.0,4X))
  Q(I,J) = XQ
  TOUT(I,J) = XTOUT
  16 CONTINUE
  READ (5,17) (SIRPO(L), SITOUT(L), SITIN(L), L = 1, NUM)
  17 FORMAT(3F10.0)
  SUMY(1)=0.0
  DO 20 I = 1,8
  DO 20 J = 1,8
  IF(TOUT(I,J).EQ.0.0) GO TO 20
  X(I,J) = TOUT(I,J) - TIN

```

```

Y(I,J) = Q(I,J)/X(I,J)
SUMY(1)=SUMY(1)+Y(I,J)
20 CONTINUE
FANOR(1)=38./SUMY(1)
DO 998 L = 1, NUM
SPOSUM(L) = 0.0
STOSUM(L) = 0.0
STISUM(L) = 0.0
S2YSUM(L) = 0.0
DO 30 I = 1,8
DO 30 J = 1,8
DO 25 K = 1,5
FLOFA(I,J,K) = 0.0
SI2FLO(I,J,K) = 0.0
SIFLO(I,J,K) = 0.0
SIRFLO(I,J,K) = 0.0
RESUL2(I,J,K) = 0.0
25 CONTINUE
DO 30 M = 1,8
RESUL3(I,J,M) = 0.0
30 CONTINUE
DO 50 I = 1,8
DO 50 J = 1,8
IF(TOUT(I,J).EQ.0.0) GO TO 50
SIRTOU(I,J) = (SITOUT(L)/X(I,J))*(SITOUT(L)/X(I,J))
SIRTIN(I,J) = (SITIN(L)/X(I,J))*(SITIN(L)/X(I,J))
SPO(I,J) = Y(I,J)*SIRPO(L)* Y(I,J)* SIRPO(L)
STO(I,J) = Y(I,J)* Y(I,J)* SIRTOU(I,J)
STI(I,J) = Y(I,J)* Y(I,J)* SIRTIN(I,J)
SI2Y(I,J) = SPO(I,J) + STO(I,J) +STI(I,J)
SPOSUM(L) = SPOSUM(L) + SPO(I,J)
STOSUM(L) = STOSUM(L) + STO(I,J)
STISUM(L) = STISUM(L) + STI(I,J)
S2YSUM(L) = S2YSUM(L) + SI2Y(I,J)
A(L)=S2YSUM(L)/(SUMY(1)*SUMY(1))
50 CONTINUE
501 CONTINUE
DO 52 I=1,8
DO 52 J=1,8
IF(TOUT(I,J).EQ.0.0) GO TO 52
SI2RFL(I,J) = A(L) + SIRPO(L)* SIRPO(L) + SIRTOU(I,J)
1 + SIRTIN(I,J)
K = 1
FLOFA(I,J,K)=FANOR(1)*Y(I,J)
K = 2
SI2FLO(I,J,K) = (Y(I,J)* FANOR(1))**2*A(L)+(FANOR(1)*Y(I,J)
1* SIRPO(L)**2 + (FANOR(1)* Y(I,J)/X(I,J)* SITOUT(L))
2**2 + (FANOR(1)* Y(I,J)/X(I,J)* SITIN(L))**2
K = 3
SIFLO(I,J,K)= DSORT(SI2FLO(I,J,2))
K = 4
SIRFLO(I,J,K) = SIFLO(I,J,3)/FLOFA(I,J,1)* 100.
DO 52K=1,4
RESUL2(I,J,K) = FLOFA(I,J,K) + SI2FLO(I,J,K) + SIFLO(I,J,K)
1 + SIRFLO(I,J,K)
522 CONTINUE
52 CONTINUE
521 CONTINUE
DO 53 I=1,8

```

```

DO 53 J=1,8
DO 53 M=1,8
CONOR(I,J,M)=0.0
COP01(I,J,M)=0.0
COT01(I,J,M)=0.0
COTI1(I,J,M)=0.0
COP02(I,J,M)=0.0
COT02(I,J,M)=0.0
COTI2(I,J,M)=0.0
RESUL3(I,J,M)=0.0
53 CONTINUE
531 CONTINUE
DO 55 I=1,8
DO 55 J=1,8
IF(TOUT(I,J).EQ.0.0) GO TO 55
M = 1
CONOR(I,J,M) = A(L)/SI2RFL(I,J)* 100.
M = 2
COP01(I,J,M)=SIRPO(L) * SIRPO(L)/ SI2RFL(I,J)* 100.
M = 3
COT01(I,J,M) = SIRT0U(I,J)/SI2RFL(I,J)* 100.
M = 4
COTI1(I,J,M) = SIRTIN(I,J)/SI2RFL(I,J)* 100.
M = 5
COP02(I,J,M)=CONOR(I,J,1)*SPOSUM(L)/S2YSUM(L)+COP01(I,J,2)
M = 6
COT02(I,J,M)=CONOR(I,J,1)*STOSUM(L)/S2YSUM(L)+COT01(I,J,3)
M = 7
COTI2(I,J,M)=CONOR(I,J,1)*STISUM(L)/S2YSUM(L)+COTI1(I,J,4)
DO 552M=1,7
RESUL3(I,J,M) = CONOR(I,J,M) + COP01(I,J,M) + COT01(I,J,M)
1+ COTI1(I,J,M) + COP02(I,J,M) + COT02(I,J,M) + COTI2(I,J,M)
552 CONTINUE
55 CONTINUE
551 CONTINUE
WRITE(6,60) RUN(1), RUN(1)
60 FORMAT(1H1,35X,'EFFECTIVE FLOW FACTOR DISTRIBUTION #',2X,A8,15X,'R
1UN # ',A8,'PAGE 1',////)
WRITE(6,61)
61 FORMAT(1X,'EFF = CONSTANT * RELATIVE POWER / TEMPERATURE DIFFERENC
1E ACROSS THE FUEL ASSEMBLY',////)
WRITE(6,62) SIRPO(L), SITOUT(L), SITIN(L)
62 FORMAT(1X,'PARAMETERS : RELATIVE POWER STD.',5X,'=',F10.4,/14X,'OU
1TLET TEMPERATURE STD. =',F8.2,2X,'DEG. F. ',/14X,'INLET TEMPERATUR
2E STD. =',F8.2,2X,'DEG. F.',////)
WRITE(6,63) SUMY(1), FANOR(1), S2YSUM(L), SPOSUM(L), STOSUM(L),
1STISUM(L)
63 FORMAT(1X,'RESULTS: SUM OF THE RATIOS',6X,'=',2X,F14.10,/10X,'NORM
1ALIZATION FACTOR =',2X,F14.10,/10X,'SUM OF THE STD. SQUARE =',2X
2,F14.10,/10X,'CONTRIBUTION OF POWER =',2X,F14.10,/10X,'CONTRIBUTI
3ON OF T. OUT =',2X,F14.10,/10X,'CONTRIBUTION OF T. INL =',2X,F14.1
40,////)
WRITE(6,640) POWER
640 FORMAT(1H , 'THERMAL POWER =',A8,' MWT#)
WRITE(6,64) RUN(1)
64 FORMAT(1H1, 100X,'RUN #',2X,A8,2X,'PAGE 2',/)
WRITE(6, 65) SIRPO(L), SITOUT(L), SITIN(L)
65 FORMAT(1H , 'RELATIVE POWER STD.',5X,'=',F10.4,/1H , 'OUTLET TEMPERA
1TURE STD. =',F8.2,2X,'DEG. F.',/1H , 'INLET TEMPERATURE STD. =',F8

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2.2,2X,'DEG. F.',///)
WRITE(6, 66)
66 FORMAT(1H .8X,.15',13X,.14',13X,.13',13X,.12',13X,.11',13X,.10',14
1X,.9',14X,.8',//)
FORM(1)=LEFT
FORM(10)=RIGHT
DO 100 I = 1,8
DO 95 K = 1,5
DO 90 J=1,8
IF (RESUL2(I,J,K).EQ.0.0) GOTO 85
FORM(J+1) = FSPEC
GO TO 90
85 FORM(J+1) = ASPEC
RESUL2(I,J,K) = BLANKS
90 CONTINUE
WRITE(6, FORM)(RESUL2(I,J,K),J=1,8)
WRITE(6,971)COLUMK(K)
971 FORMAT(1H+,122X,A8)
IF(K.NE.2.0) GO TO 95
WRITE(6,96) COLUMI(I)
96 FORMAT(1H+,126X,A4)
95 CONTINUE
100 CONTINUE
WRITE(6, 120)
120 FORMAT(//,1X,'TABLE # 1: THE FOLLOWING VALUES INCLUDED ARE:',/,
11X,'1* EFFECTIVE FLOW FACTOR NORMALIZED TO 1 OVER THE ASSEMBLIES W
2ITH OUTLET THERMOCOUPLES',/1X,'2* SQUARE OF THE STANDARD DEVIATION
3 OF THE EFFECTIVE FLOW FACTOR',/1X,'3* STANDARD DEVIATION OF THE E
4FFECTIVE FLOW FACTOR',/1X,'4* RELATIVE STANDARD DEVIATION OF THE E
5FFECTIVE FLOW FACTOR')
WRITE(6,140) RUN(1)
140 FORMAT(1H1, 100X,'RUN #',2X,A8,2X,'PAGE 3',/)
WRITE(6,141) SIRPO(L), SITOUT(L), SITIN(L)
141 FORMAT(1H .8X,'RELATIVE POWER STD.',5X,'=',F10.4,/1H .8X,'OUTLET TEMPERA
TURE STD. =',F8.2,2X,'DEG. F.',/1H .8X,'INLET TEMPERATURE STD. =',F8
2.2,2X,'DEG. F.',///)
WRITE(6,142)
142 FORMAT(1H .8X,.15',13X,.14',13X,.13',13X,.12',13X,.11',13X,.10',14
1X,.9',14X,.8',//)
FORM(1)=LEFT
FORM(10)=RIGHT
DO 200 I = 1,5
DO 190 M = 1,8
DO 180 J=1,8
IF (RESUL3(I,J,M).EQ.0.0) GO TO 170
FORM(J+1) = FSPEC
GO TO 180
170 FORM(J+1) = ASPEC
RESUL3(I,J,M) = BLANKS
180 CONTINUE
WRITE(6,FORM)(RESUL3(I,J,M),J=1,8)
WRITE(6,191) COLUMM(M)
191 FORMAT(1H+,122X,A4)
IF(M.NE.4.0) GO TO 190
WRITE(6,192) COLUMI(I)
192 FORMAT(1H+,126X,A4)
190 CONTINUE
200 CONTINUE
WRITE(6,210) RUN(1)

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210  FORMAT(1H1, 100X,'RUN #',2X,A8,2X,'PAGE 4',/)
      WRITE (6,211) SIRPO(L), SITOUT(L), SITIN(L)
211  FORMAT(1H .,RELATIVE POWER STD.,5X,'=',F10.4,/1H .,OUTLET TEMPERA
      TURE STD. =',F8.2,2X,'DEG. F.,'/1H .,INLET TEMPERATURE STD. =',F8
      2.2,2X,'DEG. F.,'///)
      WRITE(6,212)
212  FORMAT(1H .,8X,'15',13X,'14',13X,'13',13X,'12',13X,'11',13X,'10',14
      1X,'9',14X,'8',//)
      FORM(1)=LEFT
      FORM(10)=RIGHT
      DO 300 I = 6, 8
      DO 285 M = 1,8
      DO 270 J =1, 8
      IF (RESUL3(I,J,M).EQ.0.0) GO TO 255
      FORM(J+1) = FSPEC
      GO TO 270
255  FORM (J+1) = ASPEC
      RESUL3(I,J,M) = BLANKS
270  CONTINUE
      WRITE (6,FORM)(RESUL3(I,J,M),J=1,8)
      WRITE(6,286) COLUMM(M)
286  FORMAT(1H+,122X,A4)
      IF(M.NE.4.0) GO TO 285
      WRITE (6,288) COLUMI(I)
288  FORMAT(1H+,126X,A4)
285  CONTINUE
300  CONTINUE
      WRITE(6,400)
400  FORMAT(//,1X,'TABLE # 2 THE SQUARE OF THE STANDARD DEVIATION IS MA
      IDE UP OF: ',//1X,'1* CONTRIBUTION OF NORMALIZATION FACTOR',
      2,/1X,'2* CONTRIBUTION OF POWER',/1X,'3* CONTRIBUTION OF OUTLET TEM
      PERATURE',/1X,'4* CONTRIBUTION OF INLET TEMPERATURE',/1X,'5* TOTAL
      4 CONTRIBUTION OF POWER',/1X,'6* TOTAL CONTRIBUTION OF OUTLET TEMPE
      RATURE',/1X,'7* TOTAL CONTRIBUTION OF INLET TEMPERATURE')
998  CONTINUE
      DO 450 I=1,8
      DO 450 J=1,8
      DO 450 N=1,4
      RESUL1(I,J,N)=0.0
450  CONTINUE
      DO 460 I=1,8
      DO 460 J=1,8
      IF(TOUT(I,J).EQ.0.0) GO TO 460
      N=1
      RESUL1(I,J,N)=TOUT(I,J)
      N=2
      RESUL1(I,J,N)=X(I,J)
      N=3
      RESUL1(I,J,N)=Q(I,J)
460  CONTINUE
      WRITE(6,500) RUN(1)
500  FORMAT(1H1,35X,'EFFECTIVE FLOW FACTOR DISTRIBUTION # ',A8,////1H .
      1*THESE VALUES ARE THE INPUT DATA USED FOR THE COMPUTATION,////1H
      2.8X,'15',13X,'14',13X,'13',13X,'12',13X,'11',13X,'10',14X,'9',14X,
      3'8',//)
      FORMA(1)=LEFTA
      FORMA(10)=RIGHTA
      DO 510 I=1,8
      DO 505 N=1,4

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DO 504 J=1,8
IF (RESUL1(I,J,N).EQ.0.0) GO TO 503
FORMA(J+1)=FSPECA
GO TO 504
503 FORMA(J+1)= ASPECA
RESUL1(I,J,N)=BLANKA
504 CONTINUE
WRITE(6,FORMA) (RESUL1(I,J,N),J=1,8)
WRITE(6,507) COLUMN(N)
507 FORMAT(1H+,122X,A4)
IF (N.NE.2.0) GO TO 505
WRITE(6,506) COLUMI(I)
506 FORMAT(1H+,126X,A4)
505 CONTINUE
510 CONTINUE
WRITE(6,530)
530 FORMAT(////1H , 'THE ABOVE DATA ARE: 1* OUTLET TEMPERATURE (DEG. F.
1.)',/1H ,20X,'2* TEMPERATURE DIFFERENCE ACROSS THE FUEL ASSEMBLY (
2DEG. F.)',/1H ,20X,'3* RELATIVE POWER OF THE ASSEMBLY',///)
WRITE(6,535) TIN
535 FORMAT(1H , 'INLET TEMPERATURE =',F6.2,'DEG. F.')
```

STOP  
END



SAMPLE INPUT FOR FLOFA 1  
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089
1813.5
10      522.3      38
(      ' ' )      A8.7X, F15.3.
(      ' ' )      A8.7X, F15.10.
R      P      N      M      L      K      J      H
1*     2*     3*     4*
1*     2*     3*     4*     5*     6*     7*
1*     2*     3*
1 8 0.7690      573.8
2 5 0.7366      571.6
2 6 1.0118      575.7
2 7 1.2005      588.2
3 4 0.7895      572.2
3 6 0.9347      578.5
3 7 1.0156      576.4
3 8 1.0278      574.3
4 4 1.0619      582.7
4 5 1.1784      583.7
4 6 1.1579      577.8
4 7 1.1570      583.9
5 2 0.7085      574.8
5 3 1.2356      584.7
5 4 1.1817      586.2
5 5 0.9491      575.1
5 6 0.9730      575.3
5 7 0.9850      576.6
5 8 1.0883      578.7
6 2 0.9782      573.5
6 3 0.9292      575.3
6 4 1.1633      573.4
6 5 0.9801      575.7
6 6 1.1025      574.5
7 1 0.731      566.4
7 2 1.238      586.4
7 4 1.1799      583.5
7 6 1.1365      581.1
7 7 0.9258      572.2
7 8 1.0250      576.0
8 1 0.7956      568.4
8 2 0.9572      572.5
8 3 1.1994      572.6
8 4 0.9769      575.9
8 5 1.1263      580.9
8 6 0.8549      570.3
8 7 1.0323      577.5
8 8 0.8026      569.3
0.0250 2.0      0.1
0.0250 2.5      0.1
0.0250 2.5      0.2
0.0275 2.0      0.1
0.0275 2.5      0.1
0.0275 2.0      0.2
0.0275 2.5      0.2
0.0300 2.0      0.1
0.0300 2.5      0.1
0.0300 2.5      0.2

```

EFF = CONSTANT \* RELATIVE POWER / TEMPERATURE DIFFERENCE ACROSS THE FUEL ASSEMBLY

PARAMETERS : RELATIVE POWER STD. = 0.0275  
OUTLET TEMPERATURE STD. = 2.50 DEG. F.  
INLET TEMPERATURE STD. = 0.10 DEG. F.

RESULTS: SUM OF THE RATIOS = 0.7021423057  
NORMALIZATION FACTOR = 54.1200831974  
SUM OF THE STD. SQUARE = 0.0000381581  
CONTRIBUTION OF POWER = 0.0000099162  
CONTRIBUTION OF T. OUT = 0.0000281968  
CONTRIBUTION OF T. INL = 0.0000000451

THERMAL POWER = 1813.5 MWTH

RELATIVE FLOW STD. = 0.0275  
 OUTLET TEMPERATURE STD. = 2.53 DEG. F.  
 INLET TEMPERATURE STD. = 0.10 DEG. F.

153

15	14	13	12	11	10	9	8	
							0.8081231841	1*
							0.0020859243	2* R
							0.0456708252	3*
							5.6514692551	4*
				0.8086177137	1.0254438236	0.9859053092		1*
				0.0022791886	0.0031850353	0.0022114302		2* P
				0.0472142841	0.0564361165	0.0470258458		3*
				5.8388881754	5.5075795472	4.7698136266		4*
			0.8562686510		0.9001075047	1.0159770147	1.0645004057	1*
			0.0024545168		0.0022812135	0.0030682386	0.0035680274	2* N
			0.0495430805		0.0477620511	0.0553916837	0.0597329674	3*
			5.7859271649		5.3062607332	5.4520607127	5.6113616394	4*
			0.9514919925	1.0386825088	1.1291107087	1.0165087055		1*
			0.0023082316	0.0026908359	0.0036537761	0.0025660509		2* M
			0.0480440588	0.0518732672	0.0604464729	0.0506562029		3*
			5.0493392628	4.9941408259	5.3534584711	4.9833516105		4*
	0.7303634085	1.0716470320	1.0008404118	0.9728289955	0.9935630368	0.9817363158	1.0443064990	1*
	0.0016562229	0.0028037128	0.0023707365	0.0029140631	0.0030279046	0.0028497531	0.0030553672	2* L
	0.0406967182	0.0529500973	0.0486902094	0.0539820628	0.0549809477	0.0533830786	0.0552753763	3*
	5.5721189378	4.9410016326	4.8649323921	5.5489775736	5.5337150931	5.4376188130	5.2930223366	4*
	1.0335895583	0.9498373832	1.2320526964	0.9933163585	1.1430534813			1*
	0.0034443765	0.0027569756	0.0049045168	0.0029885854	0.0040909161			2* K
	0.0586888108	0.0525059575	0.0700322552	0.0546679559	0.0639602701			3*
	5.6759577832	5.5337150931	5.6841931727	5.5035795472	5.5955623363			4*
0.3970925355	1.0452521929		1.0434033687		1.0460454856	1.0040956518	1.0336230415	1*
0.0037513297	0.0025753686		0.0027271862		0.0028933540	0.0033751735	0.0032009150	2* J
0.0571080443	0.0507480918		0.0522224679		0.0537899064	0.0580962431	0.0566561113	3*
6.3655034330	4.8551052196		5.0050123690		5.1422148615	5.7859271649	5.4813127286	4*
0.9116744	1.0319670344	1.2904896180	0.9863789044	1.0401953875	0.9639012318	1.0121043820	0.9241867824	1*
0.002849255	0.0035331065	0.0055088045	0.0029310761	0.0028744772	0.0032989409	0.0029584426	0.0031324586	2* H
0.0574188601	0.0594399437	0.0742213240	0.0541394133	0.0536141508	0.0574364074	0.0543915671	0.0559687291	3*
6.1475527217	5.759798103	5.7514080641	5.4987034807	5.1542384717	5.9587440592	5.3741064684	6.0559975753	4*

TABLE # 1: THE FOLLOWING VALUES INCLUDED ARE:  
 1\* EFFECTIVE FLOW FACTOR NORMALIZED TO 1 OVER THE ASSEMBLIES WITH OUTLET THERMOCOUPLES  
 2\* SQUARE OF THE STANDARD DEVIATION OF THE EFFECTIVE FLOW FACTOR  
 3\* STANDARD DEVIATION OF THE EFFECTIVE FLOW FACTOR  
 4\* RELATIVE STANDARD DEVIATION OF THE EFFECTIVE FLOW FACTOR

RELATIVE POWER STD. = 0.0275  
OUTLET TEMPERATURE STD. = 2.50 DEG. F.  
INLET TEMPERATURE STD. = 0.10 DEG. F.

RUN # 089 PAGE 3

15	14	13	12	11	10	9	8	
							2.4233373156	1*
							23.6778793192	2*
							73.7807344900	3*
							0.1180491752	4* P
							24.3076342601	5*
							75.5714514176	6*
							0.1209143223	7*
				2.2702625507	2.5553235939	3.4019942957		1*
			22.1822232538	24.9674904024	33.2401188354			2*
			75.4268312654	72.3614077513	63.2566761871			3*
			0.1206829300	0.1157782524	0.1012106819			4* P
			22.7721985850	25.6315448234	34.1241983929			5*
			77.1044343201	74.2496557274	65.7705686972			6*
			0.1233670949	0.1187994492	0.1052329099			7*
		2.3120140896		2.7489018203	2.6038444362	2.4581019041		1*
		22.5901681211		26.8588995842	25.4415766070	24.0175592020		2*
		74.9778532242		70.2797509939	71.8396355399	73.4068878734		3*
		0.1199645652		0.1124476016	0.1149434169	0.1174510226		4* N
		23.1909934652		27.5732593667	26.1182401864	24.6563485281		5*
		76.6863084413		72.3110429645	73.7637378330	75.2232942011		6*
		0.1226980935		0.1156976687	0.1180219805	0.1203572707		7*
			3.0357590441	3.1032361940	2.7006451556	3.1166880759		1*
			29.6617168087	30.3210708186	26.3873945905	30.4524561217		2*
			67.1950121277	66.4693919602	70.7986823531	66.3247362245		3*
			0.1075120194	0.1063510271	0.1132778918	0.1061195780		4* M
			30.4506224562	31.1274618185	27.0892138757	31.2623928751		5*
			69.4387763017	68.7625181524	72.7943157199	68.6278026406		6*
			0.1111012421	0.1100200290	0.1164709044	0.1098044842		7*
	2.4928470751	3.1703441318	3.2702637659	2.5136827324	2.5275677771	2.6176940269	2.7626695920	1*
	24.3570464300	30.9767173407	31.9530095450	24.5606769371	24.6962445770	25.5768078330	26.9934213757	2*
	73.0332532897	65.7477421401	64.6732498899	72.8091956175	72.6598818350	71.6907030153	70.1316983150	3*
	0.1168532053	0.1051963874	0.1034771992	0.1164947130	0.1162558109	0.1147051248	0.1122107173	4* L
	25.0048650174	31.8005977455	32.8028561620	25.2138601071	25.3531360670	26.2571605189	27.7113590024	5*
	74.8753344475	69.0904575225	67.0998001577	74.6666732158	74.5276197414	73.6250394180	72.1731639353	6*
	0.1198005351	0.1089447320	0.1073436803	0.1194666771	0.1192441916	0.1178000631	0.1154770623	7*

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RELATIVE POWER STD. = 0.0275  
 OUTLET TEMPERATURE STD. = 2.50 DEG. F.  
 INLET TEMPERATURE STD. = 0.10 DEG. F.

155

15	14	13	12	11	10	9	8	
	2.4024706336	2.5275677771	2.3955141674	2.5553235939	2.4720026070			1*
	23.4739986074	24.6962945770	23.4060285461	24.9674904024	24.1533798342			2*
	74.0051225629	72.6598818350	74.0799293994	72.3614077513	73.2574057097			3*
	0.1184081961	0.1162558109	0.1185278870	0.1157782524	0.1172118491			4* K
	24.0983309814	25.3531360670	24.0285531365	25.6315449234	24.7957815496			5*
	75.7864273460	74.5276197414	75.8500867248	74.2496557274	75.0840839162			6*
	0.1212486726	0.1192441916	0.1213601388	0.1187994492	0.1201345343			7*
1.9099247923	3.2835157938		3.0897695391		2.9270892358	2.3120140896	2.5761268214	1*
19.6614462555	32.0874920722		30.1894411715		28.5999286255	22.5901681211	25.1707540445	2*
79.3017455587	64.5307430052		66.6142065589		68.3636003781	74.9778532242	72.1376988160	3*
0.1248827935	0.1032491988		0.1065827305		0.1093817606	0.1199645652	0.1154203181	4* J
19.1577803159	32.9357824540		30.9923825787		29.3605941445	23.1909934652	25.8402146705	5*
80.7130797581	66.9570862081		68.9973816107		70.5265633542	76.6863084413	74.0413192687	6*
0.1291405260	0.1071313379		0.1102358106		0.1128425014	0.1226980935	0.1184661109	7*
2.0480090766	2.1328911666	2.3398501068	2.5691937830	2.9134487610	2.1798516421	2.6799325813	2.1104011544	1*
20.0106346947	22.7941533314	22.8621475664	25.1030178904	28.4666506237	21.2989386607	26.1850167082	20.6202536123	2*
77.9168462659	74.7533501417	74.6785167000	72.2122537207	68.5102841612	76.3990711832	71.0214164442	77.1459117744	3*
0.1245059538	0.1196053602	0.1194856267	0.1155396067	0.1096164547	0.1222385139	0.1136342663	0.1234334588	4* H
20.5428528000	23.4004040718	23.4702066834	25.7706717709	29.2237713788	21.8653188215	26.8814533877	21.1686856074	5*
79.3302189499	76.4772324063	76.4075412506	74.1107510275	70.6631675532	78.0098653939	73.0017438222	78.7053857754	6*
0.1249243502	0.1223635719	0.1227520660	0.1185772016	0.1130610681	0.1248157846	0.1168027901	0.1259286172	7*

TABLE # 2 THE SQUARE OF THE STANDARD DEVIATION IS MADE UP OF:

- 1\* CONTRIBUTION OF NORMALIZATION FACTOR
- 2\* CONTRIBUTION OF POWER
- 3\* CONTRIBUTION OF OUTLET TEMPERATURE
- 4\* CONTRIBUTION OF INLET TEMPERATURE
- 5\* TOTAL CONTRIBUTION OF POWER
- 6\* TOTAL CONTRIBUTION OF OUTLET TEMPERATURE
- 7\* TOTAL CONTRIBUTION OF INLET TEMPERATURE

EFFECTIVE FLOW FACTOR DISTRIBUTION # 089

THESE VALUES ARE THE INPUT DATA USED FOR THE COMPUTATION

156

15	14	13	12	11	10	9	8	
							573.800	1*
							51.500	2* R
							0.769	3*
				571.600	575.700	588.200		1*
				49.300	53.400	65.900		2* P
				0.737	1.012	1.200		3*
			572.200		578.500	576.400	574.300	1*
			49.900		56.200	54.100	52.000	2* N
			0.789		0.935	1.016	1.023	3*
			582.700	583.700	577.800	583.900		1*
			60.400	61.400	55.500	61.600		2* M
			1.062	1.178	1.158	1.157		3*
	574.900	584.700	586.200	575.100	575.300	576.600	578.700	1*
	52.500	62.400	63.900	52.800	53.000	54.300	56.400	2* L
	0.709	1.236	1.182	0.949	0.973	0.985	1.088	3*
	573.500	575.300	573.400	575.700	574.500			1*
	51.200	53.000	51.100	53.400	52.200			2* K
	0.978	0.929	1.163	0.980	1.103			3*
566.400	586.400		583.500		581.100	572.200	576.000	1*
44.100	64.100		61.200		58.800	49.900	53.700	2* J
0.731	1.238		1.180		1.137	0.926	1.026	3*
568.400	572.500	572.600	575.900	580.900	570.300	577.500	569.300	1*
46.100	50.200	50.300	53.600	58.600	48.000	55.200	47.000	2* H
0.796	0.957	1.199	0.977	1.126	0.855	1.032	0.803	3*

THE ABOVE DATA ARE: 1\* OUTLET TEMPERATURE (DEG. F.)  
 2\* TEMPERATURE DIFFERENCE ACROSS THE FUEL ASSEMBLY (DEG. F.)  
 3\* RELATIVE POWER OF THE ASSEMBLY

INLET TEMPERATURE = 522.30 DEG. F.

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C      PROGRAM FLOFA 2
C*****
C CASE EFFECTIVE FLOW FACTOR DISTRIBUTION
  IMPLICIT RFAL*8 (A-H,O-Z)
  REAL *8 LEFT, RIGHT, ASPEC, FSPEC, BLANKS
  REAL*8 LEFTA, RIGHTA, ASPECA, FSPECA, BLANKA
  DIMENSION RESUL1(8,8,5), RESUL2(8,8,5), RESUL3(8,8,8),
1SIRHIN(8,8), Q(8,8), TOUT(8,8), Y(8,8), X(8,8), SIRHOU(8,8), SPO(8
2,8), STO(8,8), STI(8,8), SI2Y(8,8), SI2RFL(8,8),
3SIFLO(8,8,5), FLOFA(8,8,5), SI2FLO(8,8,5), SIRFLO(8,8,5),
4CONOR(8,8,8), COP01(8,8,8), COT01(8,8,8), COTI1(8,8,8), COP02(8,8,
58), COT02(8,8,8), COTI2(8,8,8), DERHIN(1),
6SIRPO(10), SITOUT(10), SITIN(10), SPOSUM(10), SUMY(1), FANOR(1),
7STOSUM(10), STISUM(10), S2YSUM(10), A(10), COLUMN(5),
8FORM(10), RUN(3), FORMA(10), COLUMI(8), COLUMK(5), COLUMM(8),
9ENT(11), TEMP(11), HOUT(8,8), HIN(1), DERENT(11), DERHOJ(8,8)
  READ (5,8) RUN
 8  FORMAT(5A8)
  READ (5,9) POWER
 9  FORMAT (A8)
  READ(5,10) NUM, TIN, NUM2
10  FORMAT(I2,7X,F10.0,4X,I3)
  READ(5,11) LEFTA, RIGHTA, ASPECA, FSPECA, BLANKA
11  FORMAT(5A8)
  READ (5,12) LEFT,RIGHT, ASPEC, FSPEC, BLANKS
12  FORMAT(5A8)
  READ (5,13) (COLUMI(I), I=1,8)
13  FORMAT(8A8)
  READ (5,18) (COLUMK(K), K=1,5)
18  FORMAT(5A8)
  READ (5,19) (COLUMM(M), M=1,8)
19  FORMAT(8A8)
  READ (5,5) (COLUMN(N), N=1,5)
 5  FORMAT(5A8)
  DO 14 I=1,8
  DO 14 J=1,8
  TOUT(I,J)=0.0
  Q(I,J)=0.0
  Y(I,J) = 0.0
  X(I,J) = 0.0
  SIRHOU(I,J)=0.0
  SIRHIN(I,J)=0.0
  SPO(I,J)=0.0
  STO(I,J)=0.0
  STI(I,J)=0.0
  SI2Y(I,J) = 0.0
  HOUT(I,J)=0.0
  DERHOJ(I,J)=0.0
14  CONTINUE
  DO 16 IN = 1, NUM2
  READ (5,15) I, J, XQ, XTOUT
15  FORMAT(2(I2,1X),2(F10.0,4X))
  Q(I,J) = XQ
  TOUT(I,J) = XTOUT
16  CONTINUE
  TOUT(1,1)=TIN
  READ (5,17) (SIRPO(L), SITOUT(L), SITIN(L), L = 1, NUM)
17  FORMAT(3F10.0)
C CARDS DEFINING ENTHALPY OF H2O AS A FUNCTION OF TEMP @ P=2,000 PSIA

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DO 21 II=1,11
READ(5,22) ENT(II), TEMP(II), DERENT(II), SENT
22 FORMAT(3F10.4, 11)
21 CONTINUE
DO 23 I=1,8
DO 23 J=1,8
IF (TOUT(I,J).EQ.0.0) GO TO 23
IF (TOUT(I,J).LT.TEMP(1)) STOP
JJ=2
24 IF (TOUT(I,J) - TEMP(JJ)) 28, 27, 26
26 JJ=JJ+1
IF (JJ.LT.II) GO TO 24
STOP
27 HOUT(I,J)= ENT(JJ)
DERHOU(I,J)= DERENT(JJ)
GO TO 23
28 HOUT(I,J)= ENT(JJ-1)+(ENT(JJ)-ENT(JJ-1))/(TEMP(JJ)-TEMP(JJ-1))*(TO
IUT(I,J)-TEMP(JJ-1))
DERHOU(I,J)=DERENT(JJ-1)+(DERENT(JJ)-DERENT(JJ-1))/(TEMP(JJ)-TEMP(
1JJ-1))*(TOUT(I,J)-TEMP(JJ-1))
23 CONTINUE
231 CONTINUE
TOUT(1,1)=0.0
HIN(1)=HOUT(1,1)
HOUT(1,1)=0.0
DERHIN(1)=DERHOU(1,1)
DERHOU(1,1)=0.0
SUMY(1)=0.0
DO 20 I = 1,8
DO 20 J = 1,8
IF (TOUT(I,J).EQ.0.0) GO TO 20
X(I,J) = HOUT(I,J)-HIN(1)
Y(I,J) = Q(I,J)/X(I,J)
SUMY(1)=SUMY(1)+Y(I,J)
20 CONTINUE
201 CONTINUE
FANOR(1)= 38./ SUMY(1)
DO 998 L = 1, NUM
SPOSUM(L) = 0.0
STOSUM(L) = 0.0
STISUM(L) = 0.0
SZYSUM(L) = 0.0
DO 30 I =1,8
DO 30 J =1,8
DO 25 K = 1,5
FLOFA(I,J,K) =0.0
SI2FLO(I,J,K) =0.0
SIFLO(I,J,K) =0.0
SIRFLO(I,J,K) =0.0
RESUL2(I,J,K) = 0.0
25 CONTINUE
DO 30 M = 1,8
RESUL3(I,J,M) = 0.0
30 CONTINUE
DO 50 I = 1,8
DO 50 J = 1,8
IF (TOUT(I,J).EQ.0.0) GO TO 50
SIRHOU(I,J)=DERHOU(I,J)*DERHOU(I,J)*SITOUT(L)*SITOUT(L)/(X(I,J)*X(
1I,J))

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SIRHIN(I,J)=DERHIN(1)*DERHIN(1)*SITIN(L)*SITIN(L)/(X(I,J)*X(I,J))
SPO(I,J) = Y(I,J)*SIRPO(L)* Y(I,J)* SIRPO(L)
STO(I,J) = Y(I,J)* Y(I,J)* SIRHOU(I,J)
STI(I,J) = Y(I,J)* Y(I,J)* SIRHIN(I,J)
SI2Y(I,J) = SPO(I,J) + STO(I,J) +STI(I,J)
SPOSUM(L) = SPOSUM(L) + SPO(I,J)
STOSUM(L) = STOSUM(L) + STO(I,J)
STISUM(L) = STISUM(L) + STI(I,J)
S2YSUM(L) = S2YSUM(L) + SI2Y(I,J)
A(L) = S2YSUM(L)/(SUMY(1)*SUMY(1))
50 CONTINUE
501 CONTINUE
DO 52 I=1,8
DO 52 J=1,8
IF (TOUT(I,J).EQ.0.0) GO TO 52
SI2RFL(I,J) = A(L) + SIRPO(L)* SIRPO(L) + SIRHOU(I,J)
1 + SIRHIN(I,J)
K = 1
FLOFA(I,J,K) = FANOR(1)*Y(I,J)
K = 2
SI2FLO(I,J,K) = (Y(I,J)* FANOR(1))*2*A(L)+(FANOR(1)*Y(I,J)*SIRPO(
1L))*2+(FANOR(1)*Y(I,J)/X(I,J)*DERHOU(I,J)*SITOUT(L))*2+(FANOR(1)
2*Y(I,J)/X(I,J)*SITIN(L))*2
K = 3
SIFLO(I,J,K)= DSQRT(SI2FLO(I,J,2))
K = 4
SIRFLO(I,J,K) = SIFLO(I,J,3)/FLOFA(I,J,1)* 100.
DO 522 K=1,4
RESUL2(I,J,K) = FLOFA(I,J,K) + SI2FLO(I,J,K) + SIFLO(I,J,K)
1 + SIRFLO(I,J,K)
522 CONTINUE
52 CONTINUE
521 CONTINUE
DO 53 I=1,8
DO 53 J=1,8
DO 53 M=1,8
CONOR(I,J,M)=0.0
COP01(I,J,M)=0.0
COT01(I,J,M)=0.0
COTI1(I,J,M)=0.0
COP02(I,J,M)=0.0
COT02(I,J,M)=0.0
COTI2(I,J,M)=0.0
RESUL3(I,J,M)=0.0
53 CONTINUE
DO 55 I=1,8
DO 55 J=1,8
IF (TOUT(I,J).EQ.0.0) GO TO 55
M = 1
CONOR(I,J,M) = A(L)/SI2RFL(I,J)* 100.
M = 2
COP01(I,J,M)=SIRPO(L) * SIRPO(L)/ SI2RFL(I,J)* 100.
M = 3
COT01(I,J,M) = SIRHOU(I,J)/SI2RFL(I,J)* 100.
M = 4
COTI1(I,J,M) = SIRHIN(I,J)/SI2RFL(I,J)* 100.
M = 5
COP02(I,J,M)=CONOR(I,J,1)*SPOSUM(L)/S2YSUM(L)+COP01(I,J,2)
M = 6

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COTO2(I,J,M)=CONOR(I,J,1)*STOSUM(L)/SZYSUM(L)*COTO1(I,J,3)
M = 7
COTI2(I,J,M)=CONOR(I,J,1)*STISUM(L)/SZYSUM(L)*COTI1(I,J,4)
DO 552M=1,7
RESUL3(I,J,M) = CONOR(I,J,M) + COP01(I,J,M) + COTO1(I,J,M)
1+ COTI1(I,J,M) + COP02(I,J,M) + COTO2(I,J,M) + COTI2(I,J,M)
552 CONTINUE
55 CONTINUE
551 CONTINUE
WRITE(6,60) RUN(1), RUN(1)
60 FORMAT(1H1,35X,'EFFECTIVE FLOW FACTOR DISTRIBUTION #',2X,A8,15X,'R
1UN # ',A8,'PAGE 1',////)
WRITE(6,61)
61 FORMAT(1X,'EFF = CONSTANT * RELATIVE POWER / ENTHALPY DIFFERENCE A
1CROSS THE FUEL ASSEMBLY',////)
WRITE(6,62) SIRPO(L), SITOUT(L), SITIN(L)
62 FORMAT(1X,'PARAMETERS : RELATIVE POWER STD.',5X,'=',F10.4,/14X,'OU
1TLET TEMPERATURE STD. =',F8.2,2X,'DEG. F. ',/14X,'INLET TEMPERATUR
2E STD. =',F8.2,2X,'DEG. F.',////)
WRITE(6,63) SUMY(1), FANOR(1), SZYSUM(L), SPOSUM(L), STOSUM(L),
1STISUM(L)
63 FORMAT(1X,'RESULTS: SUM OF THE RATIOS',6X,'=',2X,F14.10,/10X,'NORM
1ALIZATION FACTOR =',2X,F14.10,/10X,'SUM OF THE STD. SQUARE =',2X
2,F14.10,/10X,'CONTRIBUTION OF POWER =',2X,F14.10,/10X,'CONTRIBUTI
3ON OF T. OUT =',2X,F14.10,/10X,'CONTRIBUTION OF T. INL =',2X,F14.1
40,////)
WRITE(6,640) POWER
640 FORMAT(1H , 'THERMAL POWER =',A8,' MWTH')
WRITE(6,64) RUN(1)
64 FORMAT(1H1, 100X,'RUN #',2X,A8,2X,'PAGE 2',/)
WRITE (6, 65) SIRPO(L), SITOUT(L), SITIN(L)
65 FORMAT(1H , 'RELATIVE POWER STD.',5X,'=',F10.4,/1H , 'OUTLET TEMPERA
1TURE STD. =',F8.2,2X,'DEG. F. ',/1H , 'INLET TEMPERATURE STD. =',F8
2,2,2X,'DEG. F.',/)
WRITE(6, 66)
66 FORMAT(1H ,8X,'15',13X,'14',13X,'13',13X,'12',13X,'11',13X,'10',14
1X,'9',14X,'8',/)
FORM(1)=LEFT
FORM(10)=RIGHT
DO 100 I = 1,8
DO 95 K = 1,5
DO 90 J=1,8
IF (RESUL2(I,J,K).EQ.0.0) GOTO 85
FORM(J+1) = FSPEC
GO TO 90
85 FORM(J+1) = ASPEC
RESUL2(I,J,K) = BLANKS
90 CONTINUE
WRITE(6, FORM)(RESUL2(I,J,K),J=1,8)
WRITE(6,971)COLUMK(K)
971 FORMAT(1H+,122X,A8)
IF(K.NE.2.0) GO TO 95
WRITE (6,96) COLUMI(I)
96 FORMAT(1H+,126X,A4)
95 CONTINUE
100 CONTINUE
WRITE(6, 120)
120 FORMAT(//,1X,'TABLE # 1: THE FOLLOWING VALUES INCLUDED ARE:',////
11X,'1* EFFECTIVE FLOW FACTOR NORMALIZED TO 1 OVER THE ASSEMBLIES W

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21TH OUTLET THERMOCOUPLES',/1X,'2* SQUARE OF THE STANDARD DEVIATION
3 OF THE EFFECTIVE FLOW FACTOR',/1X,'3* STANDARD DEVIATION OF THE E
4FFECTIVE FLOW FACTOR',/1X,'4* RELATIVE STANDARD DEVIATION OF THE E
5FFECTIVE FLOW FACTOR')
WRITE(6,140) RUN(1)
140 FORMAT(1H1, 100X,'RUN #',2X,A8,2X,'PAGE 3',/)
WRITE (6,141) SIRPO(L), SITOUT(L), SITIN(L)
141 FORMAT(1H ,'RELATIVE POWER STD.',5X,'=',F10.4,/1H ,'OUTLET TEMPERA
ITURE STD. =',F8.2,2X,'DEG. F.',/1H ,'INLET TEMPERATURE STD. =',F8
2.2,2X,'DEG. F.',///)
WRITE(6,142)
142 FORMAT(1H ,8X,'15',13X,'14',13X,'13',13X,'12',13X,'11',13X,'10',14
1X,'9',14X,'8',///)
FORM(1)=LEFT
FORM(10)=RIGHT
DO 200 I = 1,5
DO 190 M = 1,8
DO 180 J=1,8
IF (RESUL3(I,J,M).EQ.0.0) GO TO 170
FORM(J+1) = FSPEC
GO TO 180
170 FORM (J+1) = ASPEC
RESUL3(I,J,M) = BLANKS
180 CONTINUE
WRITE (6,FORM) (RESUL3(I,J,M),J=1,8)
WRITE(6,191) COLUMM(M)
191 FORMAT(1H+,122X,A8)
IF(M.NE.4.0) GO TO 190
WRITE (6,192) COLUMI(I)
192 FORMAT(1H+,126X,A4)
190 CONTINUE
200 CONTINUE
WRITE (6,210) RUN(1)
210 FORMAT(1H1, 100X,'RUN #',2X,A8,2X,'PAGE 4',/)
WRITE (6,211) SIRPO(L), SITOUT(L), SITIN(L)
211 FORMAT(1H ,'RELATIVE POWER STD.',5X,'=',F10.4,/1H ,'OUTLET TEMPERA
ITURE STD. =',F8.2,2X,'DEG. F.',/1H ,'INLET TEMPERATURE STD. =',F8
2.2,2X,'DEG. F.',///)
WRITE(6,212)
212 FORMAT(1H ,8X,'15',13X,'14',13X,'13',13X,'12',13X,'11',13X,'10',14
1X,'9',14X,'8',///)
FORM(1)=LEFT
FORM(10)=RIGHT
DO 300 I = 6, 8
DO 285 M = 1,8
DO 270 J = 1, 8
IF (RESUL3(I,J,M).EQ.0.0) GO TO 255
FORM(J+1) = FSPEC
GO TO 270
255 FORM (J+1) = ASPEC
RESUL3(I,J,M) = BLANKS
270 CONTINUE
WRITE (6,FORM) (RESUL3(I,J,M),J=1,8)
WRITE(6,286) COLUMM(M)
286 FORMAT(1H+,122X,A8)
IF(M.NE.4.0) GO TO 285
WRITE (6,288) COLUMI(I)
288 FORMAT(1H+,126X,A4)
285 CONTINUE

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300 CONTINUE
WRITE(6,400)
400 FORMAT(//,1X,'TABLE # 2 THE SQUARE OF THE STANDARD DEVIATION IS MADE UP OF: ',//1X,'1* CONTRIBUTION OF NORMALIZATION FACTOR',2,/,1X,'2* CONTRIBUTION OF POWER',/,1X,'3* CONTRIBUTION OF OUTLET TEMPERATURE',/,1X,'4* CONTRIBUTION OF INLET TEMPERATURE',/,1X,'5* TOTAL CONTRIBUTION OF POWER',/,1X,'6* TOTAL CONTRIBUTION OF OUTLET TEMPERATURE',/,1X,'7* TOTAL CONTRIBUTION OF INLET TEMPERATURE')
998 CONTINUE
DO 450 I=1,8
DO 450 J=1,8
DO 450 N=1,5
RESUL1(I,J,N)=0.0
450 CONTINUE
DO 460 I=1,8
DO 460 J=1,8
IF(TOUT(I,J).EQ.0.0) GO TO 460
N=1
RESUL1(I,J,N)=TOUT(I,J)
N=2
RESUL1(I,J,N)=HOUT(I,J)
N=3
RESUL1(I,J,N)=X(I,J)
N=4
RESUL1(I,J,N)=O(I,J)
460 CONTINUE
WRITE(6,500) RUN(1)
500 FORMAT(1H1,35X,'EFFECTIVE FLOW FACTOR DISTRIBUTION # ',A8,//1H,1,'THESE VALUES ARE THE INPUT DATA USED FOR THE COMPUTATION',//1H,2,8X,'15',13X,'14',13X,'13',13X,'12',13X,'11',13X,'10',14X,'9',14X,'3',8',//)
FORMA(1)=LEFTA
FORMA(10)=RIGHTA
DO 510 I=1,8
DO 505 N=1,5
DO 504 J=1,8
IF(RESUL1(I,J,N).EQ.0.0) GO TO 503
FORMA(J+1)=FSPECA
GO TO 504
503 FORMA(J+1)=ASPECA
RESUL1(I,J,N)=BLANKA
504 CONTINUE
WRITE(6,FORMA) (RESUL1(I,J,N),J=1,8)
WRITE(6,507) COLUMN(N)
507 FORMAT(1H+,122X,A8)
IF(N.NE.2.0) GO TO 505
WRITE(6,506) COLUMI(I)
506 FORMAT(1H+,126X,A4)
505 CONTINUE
510 CONTINUE
WRITE(6,530)
530 FORMAT( /1H ,'THE ABOVE DATA ARE: 1*OUTLET TEMPERATURE (DEG. F. 1) ',/1H ,20X,'2* OUTLET ENTHALPY (BTU/LB)',/1H ,20X,'3* ENTHALPY DIFFERENCE ACROSS THE FUEL ASSEMBLY (BTU/LB)',/1H ,20X,'4* RELATIVE POWER OF THE FUEL ASSEMBLY')
WRITE(6,535) TIN , HIN(1)
535 FORMAT(1H ,'INLET TEMPERATURE =',F6.2,'DEG. F.',10X,'INLET ENTHALPY 1 =',F10.5,'BTU/LB')
STOP
END

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SAMPLE INPUT FOR FLOFA 2  
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089
1813.5
10      522.3      38
(      ' ')      A8.7X, F15.3.
(      ' ')      A8.7X, F15.10.
R      P      N      M      L      K      J      H
1*     2*     3*     4*
1*     2*     3*     4*     5*     6*     7*
1*     2*     3*     4*
1  8  0.7690      573.8
2  5  0.7366      571.6
2  6  1.0118      575.7
2  7  1.2005      588.2
3  4  0.7895      572.2
3  6  0.9347      578.5
3  7  1.0156      576.4
3  8  1.0228      574.3
4  4  1.0619      582.7
4  5  1.1784      583.7
4  6  1.1579      577.8
4  7  1.1570      583.9
5  2  0.7085      574.8
5  3  1.2356      584.7
5  4  1.1817      586.2
5  5  0.9491      575.1
5  6  0.9730      575.3
5  7  0.9850      576.6
5  8  1.0883      578.7
6  2  0.9782      573.5
6  3  0.9292      575.3
6  4  1.1633      573.4
6  5  0.9801      575.7
6  6  1.1025      574.5
7  1  0.731      566.4
7  2  1.238      586.4
7  4  1.1799      583.5
7  6  1.1365      581.1
7  7  0.9258      572.2
7  8  1.0256      576.0
8  1  0.7956      568.4
8  2  0.9572      572.5
8  3  1.1994      572.6
8  4  0.9769      575.9
8  5  1.1263      580.9
8  6  0.8549      570.3
8  7  1.0323      577.5
8  8  0.8026      569.3
0.0250  2.0      0.1
0.0250  2.5      0.1
0.0250  2.5      0.2
0.0275  2.0      0.1
0.0275  2.5      0.1
0.0275  2.0      0.2
0.0275  2.5      0.2
0.0300  2.0      0.1

```

0.0300	2.5	0.1	
0.0300	2.5	0.2	
487.3	500.0	1.154	
498.9	510.0	1.170	
510.7	520.0	1.185	
522.6	530.0	1.205	
534.8	540.0	1.230	
547.2	550.0	1.250	
559.8	560.0	1.280	
572.8	570.0	1.315	
586.1	580.0	1.350	
599.8	590.0	1.395	
614.0	600.0	1.450	1

EFF = CONSTANT \* RELATIVE POWER / ENTHALPY DIFFERENCE ACROSS THE FUEL ASSEMBLY

PARAMETERS : RELATIVE POWER STD. = 0.0275  
OUTLET TEMPERATURE STD. = 2.50 DEG. F.  
INLET TEMPERATURE STD. = 0.10 DEG. F.

RESULTS: SUM OF THE RATIOS = 0.5593390775  
NORMALIZATION FACTOR = 67.9373237565  
SUM OF THE STD. SQUARE = 0.0000266880  
CONTRIBUTION OF POWER = 0.0000062919  
CONTRIBUTION OF T. OUT = 0.0000203703  
CONTRIBUTION OF T. INL = 0.0000000258

THERMAL POWER = 1813.5 MWT

RELATIVE POWER STD. = 0.0275  
 OUTLET TEMPERATURE STD. = 2.50 DEG. F.  
 INLET TEMPERATURE STD. = 0.10 DEG. F.

15	14	13	12	11	10	9	8	
							0.8110250705	1*
							0.0023031205	2* R
							0.0479908377	3*
							5.9173063104	4*
				0.8138204400	1.0268132197	0.9721296014		1*
				0.0024683384	0.0035100525	0.0024107233		2* P
				0.0496823756	0.0592456957	0.0490991172		3*
				6.1048326107	5.7698610201	5.0506760754		4*
			0.8610913180		0.8985823359	1.0165325379	1.0676730085	1*
			0.0027155779		0.0025085277	0.0033792632	0.0039375729	2* N
			0.0521112068		0.0500852040	0.0581314304	0.0627500826	3*
			6.0517631241		5.5738024212	5.7186000676	5.8772753546	4*
			0.9447453458	1.0299148654	1.1280185150	1.0076594568		1*
			0.0025276801	0.0029436742	0.0040197857	0.0028066271		2* N
			0.0502760386	0.0542556372	0.0634017800	0.0529776096		3*
			5.3216497824	5.2679730131	5.6206329187	5.2574914320		4*
	0.7321032729	1.0612039801	0.9892127048	0.9748029205	0.9953474676	0.9820557946	1.0423237015	1*
	0.0018268109	0.0030643350	0.0025879420	0.0032132487	0.0033326212	0.0031381078	0.0033593876	2* L
	0.0427412080	0.0553564358	0.0508718197	0.0566855246	0.0577288594	0.0560188166	0.0579602244	3*
	5.8381391776	5.2163803436	5.1426573365	5.8150753727	5.7998700253	5.7042397110	5.5606741283	4*
	1.0383375707	0.9505414870	1.2370899073	0.9946428509	1.1461850315			1*
	0.0038045134	0.0030393357	0.0054179587	0.0032935559	0.0045136641			2* K
	0.0616307380	0.0551301708	0.0736067840	0.0573895101	0.0671838086			3*
	5.9417563595	5.7998700253	5.9499947099	5.7698610201	5.8615150901			4*
0.0081932318	1.0328548937		1.0348737161		1.0409972826	1.0097509084	1.0346512517	1*
0.0036210956	0.0078109010		0.0025840219		0.0031742564	0.0037341550	0.0035365195	2* J
0.0601755432	0.0530179305		0.0546262016		0.0563405398	0.0611077331	0.0594686426	3*
6.6259750410	5.1331441511		5.2785379318		5.4121697292	6.0517631241	5.7476992839	4*
0.9435772355	1.0373533419	1.2970826016	0.9874716795	1.0354796978	0.9718486342	1.0114468158	0.9328263057	1*
0.0036595361	0.0039073359	0.0060915128	0.0032295954	0.0031543347	0.0036601563	0.0032555080	0.0034770403	2* M
0.060490996	0.0625086867	0.0780481444	0.0568295291	0.0561634642	0.0604922254	0.0573570593	0.0599664338	3*
6.4111444497	6.0257954454	6.0172069484	5.755050742	5.4239078063	6.2251695639	5.6411329160	6.3212661828	4*

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TABLE # 1: THE FOLLOWING VALUES INCLUDED ARE:

- 1\* EFFECTIVE FLOW FACTOR NORMALIZED TO 1 OVER THE ASSEMBLIES WITH OUTLET THERMOCOUPLES
- 2\* SQUARE OF THE STANDARD DEVIATION OF THE EFFECTIVE FLOW FACTOR
- 3\* STANDARD DEVIATION OF THE EFFECTIVE FLOW FACTOR
- 4\* RELATIVE STANDARD DEVIATION OF THE EFFECTIVE FLOW FACTOR





RELATIVE POWER STD. = 0.0275  
 OUTLET TEMPERATURE STD. = 2.50 DEG. F.  
 INLET TEMPERATURE STD. = 0.10 DEG. F.

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	15	14	13	12	11	10	9	8	
		2.4155121695	2.5351691106	2.4088349190	2.5616124690	2.4821174008			1*
		21.4145946175	22.4753963676	21.3553878365	22.7098284451	22.0050694762			2*
		76.0721250275	74.8940779203	76.1378629299	74.6337331670	75.4163870086			3*
		0.0977781855	0.0953566015	0.0979143146	0.0948259189	0.0964261144			4* K
		21.9840583140	23.0730800153	21.9232873250	23.3137462974	22.5902458165			5*
		77.9158262150	76.8291103159	77.9764675360	76.5889491294	77.3109263354			6*
		0.1001154710	0.0978096688	0.1002451391	0.0973045732	0.0988278481			7*
	1.9423218442	3.2366434747		3.0607639023		2.9114562754	2.3284893594	2.5814074680	1*
	17.2200743508	28.6942771147		27.1350268523		25.8113486478	20.6430888852	22.8953198729	2*
	80.7297309949	67.9881041648		69.7195773201		71.1893958559	76.9238609300	74.4388429631	3*
	0.1077623101	0.0809752459		0.0846319253		0.0877992210	0.0995603254	0.0944296960	4* J
	17.6780048016	29.4573381941		27.8566231064		26.4977445965	21.1920463525	23.4939045331	5*
	82.2123534108	70.4585547356		72.0557833276		73.4116390142	78.7061397412	76.4091679627	6*
	0.1096417877	0.0841070702		0.0875935660		0.0906163893	0.1018139064	0.0969275042	7*
	2.0747232778	2.3486121231	2.3553144971	2.5748127613	2.8988660382	2.2005555911	2.6798745726	2.1341491490	1*
	18.3933402415	20.4214360930	20.8809056052	22.8268548794	25.6997306217	19.5088993988	23.7582743424	18.9201768943	2*
	79.4270436951	76.7307549203	76.6647705583	74.5037707596	71.3133343060	78.1883289714	73.4693793949	78.8420528790	3*
	0.1048927855	0.0991449635	0.0990099394	0.0945615997	0.0880690341	0.1022160387	0.0924716901	0.1036210777	4* H
	18.8424706003	21.3751876410	21.4361872841	23.4338847919	26.3831583350	20.0276955955	24.3900733034	19.4233173131	5*
	81.1062998100	78.5233928435	78.4625243392	76.4490621813	73.5259676450	79.8679959075	75.5148619201	80.4709965747	6*
	0.1059003145	0.1014195155	0.1012983767	0.0970530268	0.0908740200	0.1043453290	0.0950647765	0.1056861122	7*

TABLE # 2 THE SQUARE OF THE STANDARD DEVIATION IS MADE UP OF:

- 1\* CONTRIBUTION OF NORMALIZATION FACTOR
- 2\* CONTRIBUTION OF POWER
- 3\* CONTRIBUTION OF OUTLET TEMPERATURE
- 4\* CONTRIBUTION OF INLET TEMPERATURE
- 5\* TOTAL CONTRIBUTION OF POWER
- 6\* TOTAL CONTRIBUTION OF OUTLET TEMPERATURE
- 7\* TOTAL CONTRIBUTION OF INLET TEMPERATURE

EFFECTIVE FLOW FACTOR DISTRIBUTION # 089

THESE VALUES ARE THE INPUT DATA USED FOR THE COMPUTATION

15	14	13	12	11	10	9	8	
							573.800	1*
							577.854	2* R
							64.417	3*
							0.769	4*
				571.600	575.700	588.200		1*
				574.928	580.381	597.334		2* P
				61.491	66.944	83.877		3*
				0.737	1.012	1.200		4*
			572.200		578.500	576.400	574.300	1*
			575.726		584.105	581.312	578.519	2* N
			62.289		70.668	67.875	65.082	3*
			0.789		0.935	1.016	1.023	4*
			582.700	583.700	577.800	583.900		1*
			589.799	591.169	583.174	591.443		2* M
			76.362	77.732	69.737	78.006		3*
			1.062	1.178	1.158	1.157		4*
	574.800	584.700	586.200	575.100	575.300	576.600	578.700	1*
	579.184	592.539	594.594	579.583	579.849	581.578	584.371	2* L
	65.747	79.102	81.157	66.146	66.412	68.141	70.934	3*
	0.709	1.236	1.182	0.949	0.973	0.985	1.088	4*
	573.500	575.300	573.400	575.700	574.500			1*
	577.455	579.849	577.322	580.381	578.785			2* K
	64.018	66.412	63.885	66.944	65.348			3*
	0.978	0.929	1.163	0.980	1.103			4*
566.400	586.400		583.500		581.100	572.200	576.000	1*
568.120	594.868		590.895		587.607	575.726	580.780	2* J
54.683	81.431		77.458		74.170	62.289	67.343	3*
0.731	1.238		1.180		1.137	0.926	1.026	4*
568.400	572.500	572.600	575.900	580.900	570.300	577.500	565.300	1*
570.720	574.125	576.258	580.647	587.333	573.199	582.775	571.870	2* H
57.283	62.688	62.821	67.210	73.896	59.762	69.338	58.453	3*
0.796	0.957	1.199	0.977	1.126	0.855	1.032	0.803	4*

THE ABOVE DATA ARE: 1\*OUTLET TEMPERATURE (DEG. F.)  
 2\* JUTLET ENTHALPY (BTU/LB)  
 3\* ENTHALPY DIFFERENCE ACROSS THE FUEL ASSEMBLY (BTU/LB)  
 4\* RELATIVE POWER OF THE FUEL ASSEMBLY  
 INLET TEMPERATURE = 572.300 DEG. F. INLET ENTHALP = 513.437008 BTU/LB

PROGRAM FLOFA 3  
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C. CASE EFFECTIVE FLOW FACTOR DISTRIBUTION

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IMPLICIT REAL*8 (A-H,O-Z)
REAL*8 LEFT, RIGHT, ASPEC, FSPEC, BLANKS
REAL*8 LEFTA, RIGHTA, ASPECA, FSPECA, BLANKA
DIMENSION PFSUM1(8,8,7), PFSUM2(8,8,5), PFSUM3(8,8,8)
1 STPTIN(8,8), O(8,8), TOUT(8,8), Y(8,8), X(8,8), STRTOU(8,8), SPO(8
2,8), STO(8,8), STI(8,8), SI2Y(8,8), SI2PEL(8,8),
3 STFLO(8,8,5), FLOFA(8,8,5), SI2FLO(8,8,5), SI2PELO(8,8,5),
4 CONOP(8,8,8), COP01(8,8,8), COT01(8,8,8), COT11(8,8,8), COP02(8,8
5,8), COT02(8,8,8), COT12(8,8,8),
6 SITRPO(8,8), SITOUT(8,8), SITIN(8,8), SPOSUM(1), SIMY(1), FANOP(1),
7 STOSUM(1), STISUM(1), SZYSUM(1), A(1), COLUMN(7),
8 REFORM(10), RUM(3), FORMA(10), COLUMI(8), COLUMK(5), COLUMM(8)
9 READ (5,8) RUM
10 FORMAT(5A8)
11 READ (5,9) POWER
12 FORMAT(1A8)
13 READ(5,10) NUM2, ITN
14 FORMAT(I2,7X,F10.0)
15 READ(5,11) LEFTA, RIGHTA, ASPECA, FSPECA, BLANKA
16 FORMAT(5A8)
17 READ (5,12) LEFT,RIGHT, ASPEC, FSPEC, BLANKS
18 FORMAT(5A8)
19 READ (5,13) (COLUMI(I), I=1,8)
20 FORMAT(8A8)
21 READ (5,14) (COLUMK(K), K=1,5)
22 FORMAT(5A8)
23 READ (5,15) (COLUMM(M), M=1,8)
24 FORMAT(8A8)
25 READ (5,5) (COLUMN(N), N=1,7)
26 FORMAT(7A8)
27 DO 14 I=1,8
28 DO 14 J=1,8
29 TOUT(I,J)=0.0
30 O(I,J)=0.0
31 Y(I,J) = 0.0
32 X(I,J) = 0.0
33 STRTOU(I,J)=0.0
34 STPTIN(I,J)=0.0
35 SPO(I,J)=0.0
36 STO(I,J)=0.0
37 STI(I,J)=0.0
38 SI2Y(I,J) = 0.0
39 CONTINUE
40 DO 16 IN = 1, NUM2
41 READ (5,15) I, J, X0, XTOUT, XSTRPO, XSITOU, XSITIN
42 FORMAT(2(I2,1X),5(F10.0,2X))
43 Q(I,J) = X0
44 TOUT(I,J) = XTOUT
45 STRPO(I,J)=XSTRPO
46 SITOUT(I,J)=XSITOU
47 SITIN(I,J)=XSITIN
48 CONTINUE
49 SIMY(1)=0.0
50 DO 20 I = 1,8
51 DO 20 J = 1,8

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IF(TOUT(I,1).EQ.0.0) GO TO 20
X(I,J) = TOUT(I,J) - TIM
Y(I,J) = O(I,J)/X(I,J)
SUMY(1)=SUMY(1)+Y(I,J)
20 CONTINUE
FANOR(1)=3R./SUMY(1)
SPOSUM(1)=0.0
STOSUM(1)=0.0
STISUM(1)=0.0
SPYSUM(1)=0.0
DO 30 I = 1,R
DO 30 J = 1,Q
DO 25 K = 1,S
FLOFA(I,J,K) = 0.0
ST2FLO(I,J,K) = 0.0
SIFLO(I,J,K) = 0.0
STPFLO(I,J,K) = 0.0
RESUL2(I,J,K) = 0.0
25 CONTINUE
DO 30 M = 1,R
RESUL3(I,J,M) = 0.0
30 CONTINUE
DO 50 I = 1,R
DO 50 J = 1,Q
IF(TOUT(I,1).EQ.0.0) GO TO 50
SIRTOUT(I,J)=(SITOUT(I,J)/X(I,J))*(SITOUT(I,J)/X(I,J))
SIRTIN(I,J)=(SITIN(I,J)/X(I,J))*(SITIN(I,J)/X(I,J))
SPN(I,J)=Y(I,J)*SIRPN(I,J)*Y(I,J)*SIRPN(I,J)
STN(I,J) = Y(I,J)* Y(I,J)* SIRTOUT(I,J)
STI(I,J) = Y(I,J)* Y(I,J)* SIRTIN(I,J)
ST2Y(I,J) = SPN(I,J) + STN(I,J) + STI(I,J)
SPOSUM(1)=SPOSUM(1)+SPN(I,J)
STOSUM(1)=STOSUM(1)+STN(I,J)
STISUM(1)=STISUM(1)+STI(I,J)
SPYSUM(1)=SPYSUM(1)+ST2Y(I,J)
A(1)=SPYSUM(1)/(SUMY(1)*SUMY(1))
50 CONTINUE
501 CONTINUE
DO 52 I = 1,R
DO 52 J = 1,Q
IF(TOUT(I,1).EQ.0.0) GO TO 52
ST2PFL(I,J)=A(1)+SIRPN(I,J)+SIRPN(I,J)+SIRTOUT(I,J)+SIRTIN(I,J)
K = 1
FLOFA(I,J,K)=FANOR(1)*Y(I,J)
K = 2
ST2FLO(I,J,K)=(Y(I,J)*FANOR(1))**2*A(1)+(FANOR(1)*Y(I,J)*SIRPN(I,J)
1)**2+(FANOR(1)*Y(I,J)/X(I,J)*SITOUT(I,J))**2+(FANOR(1)*Y(I,J)/X(I
2,J)*SITIN(I,J))**2
K = 3
SIFLO(I,J,K) = DSORT(ST2FLO(I,J,2))
K = 4
STPFLO(I,J,K) = SIFLO(I,J,3)/FLOFA(I,J,1)* 100.
DO 522K=1,4
RESUL2(I,J,K) = FLOFA(I,J,K) + ST2FLO(I,J,K) + SIFLO(I,J,K)
1 + STPFLO(I,J,K)
522 CONTINUE
52 CONTINUE
521 CONTINUE
DO 53 I = 1,R
DO 53 J = 1,Q

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DO 53 M=1,8
CONOR(I,J,M)=0.0
COP01(I,J,M)=0.0
COT01(I,J,M)=0.0
COT11(I,J,M)=0.0
COP02(I,J,M)=0.0
COT02(I,J,M)=0.0
COT12(I,J,M)=0.0
RESUL3(I,J,M)=0.0
53 CONTINUE
531 CONTINUE
DO 55 I=1,8
DO 55 J=1,8
IF(TOUT(I,J).EQ.0.0) GO TO 55
M = 1
CONOR(I,J,M)=A(I)/SI2PFL(I,J)*100.
M = 2
COP01(I,J,M)=STRPO(I,J)*STRPO(I,J)/SI2PFL(I,J)*100.
M = 3
COT01(I,J,M) = SIRT01(I,J)/SI2PFL(I,J)* 100.
M = 4
COT11(I,J,M) = SIRT11(I,J)/SI2PFL(I,J)* 100.
M = 5
COP02(I,J,M)=CONOR(I,J,1)*SPOSUM(1)/SZYSUM(1)+COP01(I,J,2)
M = 6
COT02(I,J,M)=CONOR(I,J,1)*STOSUM(1)/SZYSUM(1)+COT01(I,J,3)
M = 7
COT12(I,J,M)=CONOR(I,J,1)*STISUM(1)/SZYSUM(1)+COT01(I,J,4)
DO 552 M=1,7
RESUL3(I,J,M) = CONOR(I,J,M) + COP01(I,J,M) + COT01(I,J,M)
1 + COT11(I,J,M) + COP02(I,J,M) + COT02(I,J,M) + COT12(I,J,M)
552 CONTINUE
55 CONTINUE
551 CONTINUE
WRITE(6,60) RUN(I), RUN(J)
60 FORMAT(1H1,35X,'EFFECTIVE FLOW FACTOR DISTRIBUTION #',2X,A8,15X,'R
IUN #',A8,'PAGE 1',////)
WRITE(6,61)
61 FORMAT(1X,'EFF = CONSTANT * RELATIVE POWER / TEMPERATURE DIFFERENC
E ACROSS THE FUEL ASSEMBLY',////)
WRITE(6,63) SUMY(1), FANOR(1), SZYSUM(1), SPOSUM(1), STOSUM(1),
1STISUM(1)
63 FORMAT(1X,'RESULTS: SUM OF THE RATIOS',6X,'=',2X,F14.10./10X,'NORM
LIZATION FACTOR =',2X,F14.10./10X,'SUM OF THE STD. SQUARE =',2X
2.F14.10./10X,'CONTRIBUTION OF POWER =',2X,F14.10./10X,'CONTRIBUTI
ON OF T. OUT =',2X,F14.10./10X,'CONTRIBUTION OF T. INL =',2X,F14.1
40.////)
WRITE(6,640) POWER
640 FORMAT(1H ,THERMAL POWER =',A8,' MWTH')
WRITE(6,64) RUN(I)
64 FORMAT(1H1, 100X,'RUN #',2X,A8,2X,'PAGE 2',/)
WRITE(6, 66)
66 FORMAT(14 ,9X,'15',13X,'14',13X,'13',13X,'12',13X,'11',13X,'10',14
1X,'9',14X,'8',//)
FORM(1)=LEFT
FORM(10)=RIGHT
DO 100 I = 1,8
DO 95 K = 1,5
DO 90 J=1,8
IF (RESUL2(I,J,K).EQ.0.0) GOTO 95

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FORM(J+1) = FSPEC
GO TO 90
95 FORM(J+1) = ASPEC
RESUL2(I,J,K) = BLANKS
90 CONTINUE
WRITE(6,FORM)(RESUL2(I,J,K),J=1,8)
WRITE(6,971) COLUMN(K)
071 FORMAT(1H+,122X,A8)
IF(K.NE.2,0) GO TO 95
WRITE(6,961) COLUMN(I)
96 FORMAT(1H+,126X,A4)
95 CONTINUE
100 CONTINUE
WRITE(6,120)
120 FORMAT(//,1X,'TABLE # 1: THE FOLLOWING VALUES INCLUDED ARE:'.//
11X,'1* EFFECTIVE FLOW FACTOR NORMALIZED TO 1 OVER THE ASSEMBLIES W
21TH OUTLET THERMOCOUPLES',//1X,'2* SQUARE OF THE STANDARD DEVIATION
3 OF THE EFFECTIVE FLOW FACTOR',//1X,'3* STANDARD DEVIATION OF THE E
4EFFECTIVE FLOW FACTOR',//1X,'4* RELATIVE STANDARD DEVIATION OF THE F
5EFFECTIVE FLOW FACTOR')
WRITE(6,140) RUN(1)
140 FORMAT(1H1,100X,'PIN #',2X,A8,2X,'PAGE 3',//)
WRITE(6,142)
142 FORMAT(1H ,9X,'15',13X,'14',13X,'13',13X,'12',13X,'11',13X,'10',14
1X,'9',14X,'8',//)
FORM(1)=LEFT
FORM(10)=RIGHT
DO 200 I = 1,5
DO 190 M = 1,8
DO 180 J = 1,8
IF (RESUL3(I,J,M).EQ.0,0) GO TO 170
FORM(J+1) = FSPEC
GO TO 180
170 FORM (J+1) = ASPEC
RESUL3(I,J,M) = BLANKS
180 CONTINUE
WRITE(6,FORM)(RESUL3(I,J,M),J=1,8)
WRITE(6,191) COLUMN(M)
191 FORMAT(1H+,122X,A4)
IF(M.NE.4,0) GO TO 190
WRITE(6,192) COLUMN(I)
192 FORMAT(1H+,126X,A4)
190 CONTINUE
200 CONTINUE
WRITE(6,210) RUN(1)
210 FORMAT(1H1,100X,'PIN #',2X,A8,2X,'PAGE 4',//)
WRITE(6,212)
212 FORMAT(1H ,9X,'15',13X,'14',13X,'13',13X,'12',13X,'11',13X,'10',14
1X,'9',14X,'8',//)
FORM(1)=LEFT
FORM(10)=RIGHT
DO 300 I = 6, 8
DO 285 M = 1, 8
DO 270 J = 1, 8
IF (RESUL3(I,J,M).EQ.0,0) GO TO 255
FORM(J+1) = FSPEC
GO TO 270
255 FORM (J+1) = ASPEC
RESUL3(I,J,M) = BLANKS
270 CONTINUE

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WRITE (6,F0RM) (RESUL(I,J,N),J=1,8)
WRITE (6,2R6) COLUMN(M)
284  FORMAT(1H+,122Y,A4)
      IF(M.NE.4,0) GO TO 285
WRITE (6,2R6) COLUMN(I)
288  FORMAT(1H+,126X,A4)
295  CONTINUE
300  CONTINUE
      WRITE(6,400)
400  FORMAT(//,1X,'TABLE # 2 THE SQUARE OF THE STANDARD DEVIATION IS MA
10E UP OF: ',//1X,'1* CONTRIBUTION OF NORMALIZATION FACTOR'
2./1X,'2* CONTRIBUTION OF POWER',/1X,'3* CONTRIBUTION OF OUTLET TEM
3PERATURE',/1X,'4* CONTRIBUTION OF INLET TEMPERATURE',/1X,'5* TOTAL
4 CONTRIBUTION OF POWER',/1X,'6* TOTAL CONTRIBUTION OF OUTLET TEMPE
5RATURE',/1X,'7* TOTAL CONTRIBUTION OF INLET TEMPERATURE')
      DO 450 I=1,8
      DO 450 J=1,8
      DO 450 N=1,7
      RESUL(I,J,N)=0.0
450  CONTINUE
      DO 460 I=1,8
      DO 460 J=1,8
      IF(TOUT(I,J).EQ.0,0) GO TO 460
      N=1
      RESUL(I,J,N)=TOUT(I,J)
      N=2
      RESUL(I,J,N)=X(I,J)
      N=3
      RESUL(I,J,N)=O(I,J)
      N=4
      RESUL(I,J,N)=SIRPO(I,J)
      N=5
      RESUL(I,J,N)=SITOUT(I,J)
      N=6
      RESUL(I,J,N)=SITIN(I,J)
460  CONTINUE
      WRITE(6,500) PUN(I)
500  FORMAT(1H),35X,'EFFECTIVE FLOW FACTOR DISTRIBUTION # ',A8,27X,'PAG
IF 5',//1H,' THESE VALUES ARE THE INPUTS USED FOR THE COMPUTATION',
2/1H',A8,'15',13X,'14',13X,'13',13X,'12',13X,'11',13X,'10',14X,'09',
314X,'08',//)
      FORMA(1)=LEFTA
      FORMA(10)=RIGHTA
      DO 510 I=1,5
      DO 505 N=1,7
      DO 504 J=1,8
      IF(RESUL(I,J,N).EQ.0,0) GO TO 503
      FORMA(J+1)=FSPECA
      GO TO 504
503  FORMA(J+1)=ASPECA
      RESUL(I,J,N)=RLANKA
504  CONTINUE
      WRITE(6,F0RMA) (RESUL(I,J,N),J=1,8)
      WRITE(6,507) COLUMN(N)
507  FORMAT(1H+,122X,A4)
      IF(N.NE.3) GO TO 505
      WRITE(6,506) COLUMN(I)
506  FORMAT(1H+,126X,A4)
505  CONTINUE
510  CONTINUE

```



```

WRITE(6,520) RIIN(1)
520 FORMAT(1H), 100X,'RIIN #',2X,A8,2X,'PAGE #',/)
WRITE(6,521)
FORMA(1)=LEFTA
FORMA(10)=RIGHTA
DO 610 I=6,8
DO 605 N=1,7
DO 604 J=1,8
IF(PFSILI(T,J,N).EQ.0.0) GO TO 603
FORMA(J+1)=FSPECA
GO TO 604
603 FORMA(J+1)=ASPECA
PFSILI(T,J,N)=RLANKA
604 CONTINUE
WRITE(6,FORMA) (PFSILI(T,J,N),J=1,8)
WRITE(6,607) COLUMN(N)
607 FORMAT(1H+,122Y,A4)
IF(N.NE.3) GO TO 605
WRITE(6,606) COLUMN(T)
606 FORMAT(1H+,126Y,A4)
605 CONTINUE
610 CONTINUE
WRITE(6,530)
530 FORMAT(/1H ,THE ABOVE DATA ARE: 1* OUTLET TEMPERATURE (DEG. F.
1) ,/1H ,20X, 2* TEMPERATURE DIFFERENCE ACROSS THE FUEL ASSEMBLY (D
2EG. F.) ,/1H ,20X, 3* RELATIVE POWER OF THE ASSEMBLY ,/1H ,20X, 4*
3 RELATIVE POWER UNCERTAINTY ,/1H ,20X, 5* OUTLET TEMPERATURE UNCE
4RTAINTY (DEG. F.) ,/1H ,20X, 6* INLET TEMPERATURE UNCERTAINTY
5 (DEG. F.) ,/1H ,NOTE: THE UNCERTAINTIES ARE RELATED TO A ONE SIG
6MA CONFIDENCE LEVEL ,/)
WRITE(6,535) TIN
535 FORMAT(1H ,INLET TEMPERATURE =',F6.2,'DEG. F. )
STOP
END

```

TABULAT FOR FLOFA 3  
\*\*\*\*\*

009		1913.5		522.3		10.7%		F15.5.		10.7%		F15.10.	
D	D	M	M	L	K	J	H						
1*	2*	3*	4*	5*	6*	7*							
1*	2*	3*	4*	5*	6*								
1	8	0.7600	573.8	0.04001	2.14		0.1						
2	5	0.7366	571.6	0.05506	2.14		0.1						
2	6	1.0118	575.7	0.05539	2.14		0.1						
2	7	1.2005	588.2	0.03157	2.14		0.1						
3	4	0.7805	572.2	0.04863	2.14		0.1						
3	6	0.9347	578.5	0.03029	2.14		0.1						
3	7	1.0156	576.4	0.02360	2.14		0.1						
3	8	1.0228	574.3	0.03057	2.14		0.1						
4	4	1.0619	582.7	0.03095	2.14		0.1						
4	5	1.1784	583.7	0.02309	2.14		0.1						
4	6	1.1579	577.8	0.02859	2.14		0.1						
4	7	1.1570	583.9	0.02331	2.14		0.1						
5	2	0.7085	574.8	0.04955	2.14		0.1						
5	3	1.2356	584.7	0.03087	2.14		0.1						
5	4	1.1817	586.2	0.02382	2.14		0.1						
5	5	0.9491	575.1	0.02143	2.14		0.1						
5	6	0.9730	575.3	0.02336	2.14		0.1						
5	7	0.9850	576.6	0.02332	2.14		0.1						
5	8	1.0883	578.7	0.04010	2.14		0.1						
6	2	0.9782	573.5	0.04748	2.14		0.1						
6	3	0.9292	575.3	0.02993	2.14		0.1						
6	4	1.1633	573.4	0.02341	2.14		0.1						
6	5	0.9801	575.7	0.02327	2.14		0.1						
6	6	1.1025	574.5	0.02314	2.14		0.1						
7	1	0.731	566.4	0.05745	2.14		0.1						
7	2	1.238	586.4	0.02655	2.14		0.1						
7	4	1.1799	583.5	0.02331	2.14		0.1						
7	6	1.1365	581.1	0.02332	2.14		0.1						
7	7	0.9258	572.2	0.02311	2.14		0.1						
7	8	1.0256	576.0	0.04029	2.14		0.1						
8	1	0.7956	568.4	0.05745	2.14		0.1						
8	2	0.9572	572.5	0.03059	2.14		0.1						
8	3	1.1994	572.6	0.02920	2.14		0.1						
8	4	0.9749	575.9	0.02891	2.14		0.1						
8	5	1.1243	580.9	0.02841	2.14		0.1						
8	6	0.8549	570.3	0.02836	2.14		0.1						
8	7	1.0323	577.5	0.02855	2.14		0.1						
8	8	0.8026	569.3	0.04002	2.14		0.1						

EFF = CONSTANT \* RELATIVE POWER / TEMPERATURE DIFFERENCE ACROSS THE FUEL ASSEMBLY

RESULTS: SUM OF THE RATIOS = 0.7021423057  
NORMALIZATION FACTOR = 54.1200831974  
SUM OF THE STD. SQUARE = 0.0000352856  
CONTRIBUTION OF POWER = 0.0000145797  
CONTRIBUTION OF T. OUT = 0.0000206608  
CONTRIBUTION OF T. INL = 0.0000000451

THERMAL POWER = 1813.5 MWTH

15 14 13 12 11 10 9 8

								0.8081231841	1*
								0.022222614	2* P
								0.0471408678	3*
								5.8333764819	4*
								0.8086177137	1*
								0.0032637682	2* P
								0.0571293986	3*
								7.0650688935	4*
								0.8562686510	1*
								0.0031378260	2*
								0.0560163013	3*
								6.5419072855	4*
								0.9514919925	1*
								0.0020739893	2* M
								0.0455081233	3*
								4.7828172673	4*
								0.7303634085	1*
								0.0022361075	2* L
								0.0472874986	3*
								6.4745163850	4*
								1.0339895583	1*
								0.0043585580	2* K
								0.0660193758	3*
								6.3849170717	4*
								0.8979925355	1*
								0.0046129682	2* J
								0.0679188355	3*
								7.5709955046	4*
								0.9340116744	1*
								0.0048257093	2* M
								0.0694673253	3*
								7.4375221612	4*

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TABLE # 1: THE FOLLOWING VALUES INCLUDED ARE:  
 1\* EFFECTIVE FLOW FACTOR NORMALIZED TO 1 OVER THE ASSEMBLIES WITH OUTLET THERMOCOUPLES  
 2\* SQUARE OF THE STANDARD DEVIATION OF THE EFFECTIVE FLOW FACTOR  
 3\* STANDARD DEVIATION OF THE EFFECTIVE FLOW FACTOR  
 4\* RELATIVE STANDARD DEVIATION OF THE EFFECTIVE FLOW FACTOR

15	14	13	12	11	10	9	8
							2.1733311619 1*
							47.0432253550 2*
							50.7426420114 3*
							0.1108013718 4* R
							47.9123031212 5*
							51.9742061674 6*
							0.0026892396 7*
							1.4338867997 1.5070777045 3.3690262657 1*
							60.7350805558 64.6024254570 46.9004451242 2*
							37.7486049108 33.8466818395 49.6231716103 3*
							0.0824277337 0.0738419990 0.1083569998 4* P
							61.3275498539 65.2251134949 48.2920936816 5*
							38.5881890991 34.6991174226 51.5952530878 6*
							0.0018333134 0.0019268835 0.0043062308 7*
							1.6723951494 2.9306916581 3.2582585132 2.6474742780 1*
							55.2585862299 37.5682535113 25.3548984615 34.5680560790 2*
							42.9751781582 59.3714116050 71.2313025805 62.6476723847 3*
							0.0938404674 0.1296432256 0.1555404458 0.1367972582 4* M
							55.9496050610 38.7791892907 26.7011919568 35.6619689519 5*
							43.9544162155 61.0974204121 73.1391117114 64.1978483305 6*
							0.0021382611 0.0037470714 0.0041658860 0.0033849604 7*
							3.1288164907 3.9279620895 3.0085604715 3.9229768074 1*
							41.8748948692 29.2595393475 34.3589107187 29.7819149253 2*
							54.8764605752 66.6669248778 62.4960626061 66.1506618923 3*
							0.1198280648 0.1455736852 0.1364862036 0.1444463750 4* M
							43.1676940709 30.8825384171 35.6020212007 31.4028541206 5*
							56.7084774780 68.9668657541 64.2576659642 68.4476837348 6*
							0.0040003863 0.0050221436 0.0038466315 0.0053157696 7*
							1.7073910494 3.2485281356 4.0597529089 3.2875114455 3.1793810194 3.2952634676 2.2922220745 1*
							58.5696527406 43.2526003674 32.1836611471 21.0942430966 24.2404448275 25.0379960675 51.4988768318 2*
							39.6364062793 53.3823060631 63.6176706007 75.4534854669 72.4220336308 71.5105901675 46.1082193824 3*
							0.0865499307 0.1165654338 0.1389153433 0.1647599910 0.1581405224 0.1561502973 0.1006817613 4* L
							59.2751315668 44.5948633582 33.8611150135 22.4526136449 25.5541368435 26.3995696826 52.4460026259 5*
							40.6361354969 55.2844177630 65.9947789969 77.3784230765 74.2836575979 73.4400668210 47.4503848646 6*
							0.0021830055 0.0041534451 0.0051906463 0.0042032876 0.0040550362 0.0042131991 0.0029307483 7*

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15	14	13	12	11	10	9	8	
1.7556467911	2.7514552400	3.0107326121	3.2202686226	3.1235539486				1*
55.2981877456	34.4372304572	23.0529944280	24.3633608705	23.3683501566				2*
42.8525926782	62.6744585544	73.7751777163	72.2585868863	73.3479335802				3*
0.0935727851	0.1368557424	0.1610952435	0.1577836206	0.1631623146				4* K
56.0236054160	35.5741073396	24.2970024192	25.6939472813	24.6589749225				5*
43.8805770953	64.2855190055	75.5380529286	74.1441517846	75.1768691051				6*
0.0022447035	0.0035179065	0.0038494087	0.0041173135	0.0039936578				7*
1.2486527912	3.7799384765	3.8891630719	3.6839023301	2.9227080312	2.1778273486			1*
57.5803220276	37.2276920786	29.5252124659	27.9909430494	21.8090055372	49.3935582242			2*
41.0813201411	58.8638345629	66.4405450991	68.1762851010	75.1041001411	48.3230962679			3*
0.0897050400	0.1285348820	0.1450793630	0.1488695194	0.1639972905	0.1055181594			4* J
58.0962542775	38.7895291052	31.1321801258	29.5130987929	23.0167325529	50.2934171535			5*
41.8124442023	61.0771031266	68.7177679745	70.3333215898	76.8155332928	49.5992811995			6*
0.0015964802	0.0048328862	0.0049725366	0.0047100980	0.0037369638	0.0027844976			7*
1.2938714302	2.5303581762	2.6138426023	2.8573356832	3.2309343949	2.4956796069	2.0910162730	1.0081712689	1*
59.6655324368	33.0821164187	31.1384840923	33.3664328325	36.4353494073	28.0447806890	34.2631343192	42.6996144669	2*
38.9555329551	64.2472353462	66.1033302835	63.6372733366	60.2022587329	69.3082075225	62.8088003111	55.2715335193	3*
0.0850631779	0.1402900588	0.1443430218	0.1389581477	0.1314574608	0.1513411816	0.1371497967	0.1276977449	4* H
60.2001486270	34.1276379569	32.2185006543	34.5470585742	37.7703428222	29.0759696315	35.2988056941	43.4987438977	5*
39.7131339001	65.7288367641	67.6338143636	65.3103299969	62.0940687666	70.7694993170	64.5601310091	56.3888256419	6*
0.0016542950	0.0032352201	0.0033419602	0.0036532812	0.0041339504	0.0031908699	0.0038242001	0.0024397155	7*

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TABLE # 2 THE SQUARE OF THE STANDARD DEVIATION IS MADE UP OF:

- 1\* CONTRIBUTION OF NORMALIZATION FACTOR
- 2\* CONTRIBUTION OF POWER
- 3\* CONTRIBUTION OF OUTLET TEMPERATURE
- 4\* CONTRIBUTION OF INLET TEMPERATURE
- 5\* TOTAL CONTRIBUTION OF POWER
- 6\* TOTAL CONTRIBUTION OF OUTLET TEMPERATURE
- 7\* TOTAL CONTRIBUTION OF INLET TEMPERATURE

EFFECTIVE FLOW FACTOR DISTRIBUTION # 089

THESE VALUES ARE THE INPUTS USED FOR THE COMPUTATION

15	14	13	12	11	10	9	8	
							573.80000	1*
							51.50000	2*
							0.76900	3* P
							0.04001	4*
							2.14000	5*
							0.10000	6*
				571.60000	575.70000	589.20000		1*
				49.30000	53.40000	65.90000		2*
				0.73660	1.01180	1.20050		3* P
				0.05576	0.05539	0.03157		4*
				2.14000	2.14000	2.14000		5*
				0.10000	0.10000	0.10000		6*
			572.20000		578.50000	576.40000	574.30000	1*
			49.90000		56.20000	54.10000	52.00000	2*
			0.78950		0.93470	1.01560	1.02280	3* N
			0.04863		0.03029	0.02360	0.03057	4*
			2.14000		2.14000	2.14000	2.14000	5*
			0.10000		0.10000	0.10000	0.10000	6*
			582.70000	583.70000	577.80000	583.90000		1*
			60.40000	61.40000	55.50000	51.60000		2*
			1.06190	1.17840	1.15790	1.15790		3* N
			0.03095	0.02309	0.02859	0.02331		4*
			2.14000	2.14000	2.14000	2.14000		5*
			0.10000	0.10000	0.10000	0.10000		6*
574.80000	584.70000	586.20000	575.10000	575.30000	576.60000	578.70000		1*
52.50000	62.40000	63.90000	52.80000	53.00000	54.30000	56.40000		2*
0.70850	1.23560	1.18170	0.94910	0.97300	2.98500	1.08830		3* I
0.04955	0.03087	0.02382	0.02143	0.02336	0.02332	0.14010		4*
2.14000	2.14000	2.14000	2.14000	2.14000	2.14000	2.14000		5*
0.10000	0.10000	0.10000	0.10000	0.10000	0.10000	0.10000		6*

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15	14	13	12	11	10	9	8	
	573.50000	575.30000	573.40000	575.70000	574.50000			1*
	51.20000	53.00000	51.10000	53.40000	52.20000			2*
	0.97820	0.92920	1.16330	0.98010	1.10250			3* K
	0.04748	0.02993	0.02341	0.02327	0.02314			4*
	2.14000	2.14000	2.14000	2.14000	2.14000			5*
	0.10000	0.10000	0.10000	0.10000	0.10000			6*
566.40000	566.40000		583.50000		581.10000	572.20000	576.00000	1*
44.10000	64.10000		61.20000		58.80000	49.90000	53.70000	2*
0.73100	1.23800		1.17990		1.13650	0.92580	1.02560	3* J
0.05745	0.02655		0.02331		0.02332	0.02311	0.04029	4*
2.14000	2.14000		2.14000		2.14000	2.14000	2.14000	5*
0.10000	0.10000		0.10000		0.10000	0.10000	0.10000	6*
568.40000	572.50000	572.60000	575.90000	580.90000	570.30000	577.50000	569.30000	1*
46.10000	50.20000	50.30000	53.60000	58.60000	48.00000	55.20000	47.00000	2*
0.79560	0.95720	1.19940	0.97690	1.12630	0.85490	1.03230	0.87260	3* H
0.05745	0.03059	0.02920	0.02891	0.02841	0.02836	0.02855	0.04002	4*
2.14000	2.14000	2.14000	2.14000	2.14000	2.14000	2.14000	2.14000	5*
0.10000	0.10000	0.10000	0.10000	0.10000	0.10000	0.10000	0.10000	6*

THE ABOVE DATA ARE: 1\* OUTLET TEMPERATURE (DEG. F.)  
 2\* TEMPERATURE DIFFERENCE ACROSS THE FUEL ASSEMBLY (DEG. F.)  
 3\* RELATIVE POWER OF THE ASSEMBLY  
 4\* RELATIVE POWER UNCERTAINTY  
 5\* OUTLET TEMPERATURE UNCERTAINTY (DEG. F.)  
 6\* INLET TEMPERATURE UNCERTAINTY (DEG. F.)

NOTE: THE UNCERTAINTIES ARE RELATED TO A ONE SIGMA CONFIDENCE LEVEL.

INLET TEMPERATURE = 522.30 DEG. F.



PROGRAM FLOFA 4  
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C CASE EFFECTIVE FLOW FACTOR DISTRIBUTION

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IMPLICIT REAL*8 (A-H,O-Z)
REAL*8 LEFT, RIGHT, ASPEC, FSPEC, BLANKS
REAL*8 LEFTA, RIGHTA, ASPECA, FSPECA, BLANKA
DIMENSION PFSU1(10,10,5), PFSU2(10,10,5), PFSU3(10,10,5)
1 STPHIN(10,10), O(10,10), TOUT(10,10), Y(10,10), X(10,10), STPHOU(10,10), SPO(10,10)
2 STO(10,10), STI(10,10), SI2Y(10,10), SI2PFL(10,10)
3 SFLO(10,10,5), FLOFA(10,10,5), SI2FLO(10,10,5), ST2FLO(10,10,5)
4 CONOP(10,10,10), COP01(10,10,10), COT01(10,10,10), COT11(10,10,10), COP02(10,10,10)
5 SA, COT02(10,10,10), COT12(10,10,10), DEPTH(10)
6 STPO(10,10), SITOUT(10,10), SITIN(10,10), SPOSUM(10), SUMY(10), FANOP(10)
7 STOSUM(10), STISUM(10), SPYSUM(10), A(10), COLUMN(5)
8 FOPM(10), PIN(10), FOPMA(10), COLUMI(10), COLUMK(5), COLUMM(10)
9 QENT(10), TEMP(10), HOUT(10,10), HIN(10), DEPFNT(10), DEPHOU(10,10)
10 READ (5,8) PIN
11 FORMAT(5A)
12 READ (5,9) POWER
13 FORMAT(1A)
14 READ (5,10) NUM2, TIN
15 FORMAT(I2,7Y,F10,0)
16 READ (5,11) LEFTA, RIGHTA, ASPECA, FSPECA, BLANKA
17 FORMAT(5A)
18 READ (5,12) LEFT, RIGHT, ASPEC, FSPEC, BLANKS
19 FORMAT(5A)
20 READ (5,13) (COLUMI(I), I=1,8)
21 FORMAT(8A)
22 READ (5,14) (COLUMK(K), K=1,5)
23 FORMAT(5A)
24 READ (5,15) (COLUMM(M), M=1,8)
25 FORMAT(8A)
26 READ (5,5) (COLUMN(N), N=1,5)
27 FORMAT(5A)
28 DO 14 I=1,8
29 DO 14 J=1,8
30 TOUT(I,J)=0.0
31 O(I,J)=0.0
32 Y(I,J)=0.0
33 X(I,J)=0.0
34 STPHOU(I,J)=0.0
35 STPHIN(I,J)=0.0
36 SPO(I,J)=0.0
37 STO(I,J)=0.0
38 STI(I,J)=0.0
39 SI2Y(I,J)=0.0
40 HOUT(I,J)=0.0
41 DEPHOU(I,J)=0.0
42 CONTINUE
43 DO 16 IN = 1, NUM2
44 READ (5,15) I, J, X0, XTOUT, XSPO, XSITOU, XSITIN
45 FORMAT(2(I2,1X),5(F10,0,2X))
46 O(I,J) = X0
47 TOUT(I,J) = XTOUT
48 SPO(I,J) = XSPO
49 SITOUT(I,J) = XSITOU
50 SITIN(I,J) = XSITIN
51 CONTINUE

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      TOUT(I,J)=TIM
C CAPDS DEFINING ENTHALPY OF H2O AS A FUNCTION OF TEMP @ P=2.000 PSTA
      DO 21 IT=1,11
      READ(5,22) FNT(IT), TEMP(IT), DFERENT(IT), SENT
22   FORMAT(F10.4, I1)
21   CONTINUE
      DO 23 IT=1,8
      DO 23 J=1,8
      IF(TOUT(I,J).EQ.0.0) GO TO 23
      IF(TOUT(I,J).LT.TEMP(IT)) STOP
      J.I=2
24   IF(TOUT(I,J) - TEMP(J,I)) 24, 27, 26
26   J.I=J.J+1
      IF(JJ.LT.11) GO TO 24
      STOP
27   HOUT(I,J)= FNT(JJ)
      DERHOUT(I,J)= DFERENT(JJ)
      GO TO 23
28   HOUT(I,J)= FNT(JJ-1)+(FNT(JJ)-FNT(JJ-1))/(TEMP(JJ)-TEMP(JJ-1))*(TOUT(I,J)-TEMP(JJ-1))
      DERHOUT(I,J)=DFERENT(JJ-1)+(DFERENT(JJ)-DFERENT(JJ-1))/(TEMP(JJ)-TEMP(JJ-1))*(TOUT(I,J)-TEMP(JJ-1))
23   CONTINUE
231  CONTINUE
      TOUT(1,1)=0.0
      HIN(1)=HOUT(1,1)
      HOUT(1,1)=0.0
      DERHIN(1)=DERHOUT(1,1)
      DERHOUT(1,1)=0.0
      SUMY(1)=0.0
      DO 20 IT = 1,8
      DO 20 J = 1,8
      IF(TOUT(I,J).EQ.0.0) GO TO 20
      X(I,J) = HOUT(I,J)-HIN(I)
      Y(I,J) = Q(I,J)/X(I,J)
      SUMY(1)=SUMY(1)+Y(I,J)
20   CONTINUE
201  CONTINUE
      FANOP(1) = 70./ SUMY(1)
      SPOSIUM(1)=0.0
      STOSIUM(1)=0.0
      STTSIUM(1)=0.0
      SPYSIUM(1)=0.0
      DO 30 T = 1,8
      DO 30 J = 1,8
      DO 25 K = 1,5
      FLOFA(I,J,K) = 0.0
      STEFLO(I,J,K) = 0.0
      STEFLO(I,J,K) = 0.0
      STEFLO(I,J,K) = 0.0
      STEFLO(I,J,K) = 0.0
      RESIUM(I,J,K) = 0.0
25   CONTINUE
      DO 30 M = 1,8
      RESIUM(I,J,M) = 0.0
30   CONTINUE
      DO 50 IT = 1,8
      DO 50 J = 1,8
      IF(TOUT(I,J).EQ.0.0) GO TO 50
      STPHOU(I,J)=DERHOUT(I,J)*DERHOUT(I,J)*SITOUT(I,J)*SITOUT(I,J)/(X(I,J)
1)*Y(I,J))

```

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SIPWHN(I,J)=DFPHN(1)*DFPHN(1)*SITIN(I,J)*SITIN(I,J)/(X(I,J)*Y(I,
1,J))
SPN(I,J) = Y(I,J)*SIPPN(I,J)*Y(I,J)*SIPPN(I,J)
STO(I,J) = Y(I,J)*Y(I,J)*SIPWHN(I,J)
STI(I,J) = Y(I,J)*Y(I,J)*SIPWHN(I,J)
STPY(I,J) = SPN(I,J) + STO(I,J) + STI(I,J)
SPOSUM(1)=SPOSUM(1)+SPN(I,J)
STOSUM(1)=STOSUM(1)+STO(I,J)
STISUM(1)=STISUM(1)+STI(I,J)
S2YSUM(1)=S2YSUM(1)+STPY(I,J)
A(1)=S2YSUM(1)/(SUMY(1)*SUMY(1))
50 CONTINUE
501 CONTINUE
DO 521 I=1,8
DO 52 J=1,8
IF(TOUT(I,J).EQ.0.0) GO TO 52
SIPDFL(I,J)=A(1)+SIPPN(I,J)*SIPPN(I,J)+SIPWHN(I,J)+SIPWHN(I,J)
K = 1
FLOFA(I,J,K) = FANOR(1)*Y(I,J)
K = 2
SIPFLO(I,J,K)=(Y(I,J)*FANOR(1))**2*A(1)+(FANOR(1)*Y(I,J)*SIPPN(I,
1))**2+(FANOR(1)*Y(I,J)/X(I,J)*DFPHN(I,J)*SITOUT(I,J))**2+(FANOR(1)
2)*Y(I,J)/X(I,J)*SITIN(I,J)**2
K = 3
SIFLO(I,J,K) = DSORT(SIPFLO(I,J,2))
K = 4
SIPFLO(I,J,K) = SIFLO(I,J,3)/FLOFA(I,J,1)*100.
DO 522K=1,4
RESUL2(I,J,K) = FLOFA(I,J,K) + SIPFLO(I,J,K) + SIFLO(I,J,K)
1 + SIPFLO(I,J,K)
522 CONTINUE
52 CONTINUE
521 CONTINUE
DO 53 I=1,8
DO 53 J=1,8
DO 53 M=1,8
CONOR(I,J,M)=0.0
CORO1(I,J,M)=0.0
COTO1(I,J,M)=0.0
COTI1(I,J,M)=0.0
CORO2(I,J,M)=0.0
COTO2(I,J,M)=0.0
COTI2(I,J,M)=0.0
RESUL3(I,J,M)=0.0
53 CONTINUE
DO 55 I=1,8
DO 55 J=1,8
IF(TOUT(I,J).EQ.0.0) GO TO 55
M = 1
CONOR(I,J,M)=A(1)/SIPDFL(I,J)*100.
M = 2
CORO1(I,J,M)=SIPPN(I,J)*SIPPN(I,J)/SIPDFL(I,J)*100.
M = 3
COTO1(I,J,M) = SIPWHN(I,J)/SIPDFL(I,J)*100.
M = 4
COTI1(I,J,M) = SIPWHN(I,J)/SIPDFL(I,J)*100.
M = 5
CORO2(I,J,M)=CONOR(I,J,1)+SPOSUM(1)/S2YSUM(1)+CORO1(I,J,2)
M = 6
COTO2(I,J,M)=CONOR(I,J,1)+STOSUM(1)/S2YSUM(1)+COTO1(I,J,3)

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```

M = 7
COT02(I,J,M) = CONOP(I,J,1) * STISUM(1) / S2YSUM(1) + COT01(I,J,4)
DO 552 M = 1,7
RESUL3(I,J,M) = CONOP(I,J,M) + COP01(I,J,M) + COT01(I,J,M)
+ COT11(I,J,M) + COP02(I,J,M) + COT02(I,J,M) + COT12(I,J,M)
552 CONTINUE
55 CONTINUE
551 CONTINUE
WRITE(6,60) RUM(1), RUM(1)
60 FORMAT(1H,35X,'EFFECTIVE FLOW FACTOR DISTRIBUTION #',2X,A8,15X,'R
UM #',A8,'PAGE 1',////)
WRITE(6,61)
61 FORMAT(1X,'EFF = CONSTANT * RELATIVE POWER / ENTHALPY DIFFERENCE A
ROSS THE FUEL ASSEMBLY',////)
WRITE(6,63) SUMY(1), FANOP(1), S2YSUM(1), SPOSUM(1), STOSUM(1),
STISUM(1)
63 FORMAT(1X,'RESULTS: SUM OF THE RATIOS',6X,'=',2X,F14,10./10X,'NORM
LIZATION FACTOR =',2X,F14,10./10X,'SUM OF THE STD. SQUARE =',2X
2.F14,10./10X,'CONTRIBUTION OF POWER =',2X,F14,10./10X,'CONTRIBUTI
ON OF T. OUT =',2X,F14,10./10X,'CONTRIBUTION OF T. IN =',2X,F14,1
40,////)
WRITE(6,640) POWER
640 FORMAT(1H,'THERMAL POWER =',A8,' MWTH')
WRITE(6,64) RUM(1)
64 FORMAT(1H),100X,'RUM #',2X,A8,2X,'PAGE 2',/)
WRITE(6,66)
66 FORMAT(1H,9X,'15',13X,'14',13X,'13',13X,'12',13X,'11',13X,'10',14
1X,'9',14X,'8',/)
FORM(1) = LEFT
FORM(10) = RIGHT
DO 100 I = 1,8
DO 95 K = 1,5
DO 90 J = 1,8
IF (RESUL2(I,J,K).EQ.0.0) GOTO 85
FORM(J+1) = FSPEC
GO TO 90
85 FORM(J+1) = ASPEC
RESUL2(I,J,K) = BLANKS
90 CONTINUE
WRITE(6,FORM) (RESUL2(I,J,K),J=1,8)
WRITE(6,97) COLUMN(K)
971 FORMAT(1H+,122X,A8)
IF (K.NE.2.0) GO TO 95
WRITE(6,96) COLUMN(I)
96 FORMAT(1H+,126X,A4)
95 CONTINUE
100 CONTINUE
WRITE(6,120)
120 FORMAT(//,1X,'TABLE # 1: THE FOLLOWING VALUES INCLUDED ARE:',////
11X,'1' EFFECTIVE FLOW FACTOR NORMALIZED TO 1 OVER THE ASSEMBLIES W
21TH OUTLET THERMOCOUPLES',/1X,'2' SQUARE OF THE STANDARD DEVIATION
3 OF THE EFFECTIVE FLOW FACTOR',/1X,'3' STANDARD DEVIATION OF THE F
4EFFECTIVE FLOW FACTOR',/1X,'4' RELATIVE STANDARD DEVIATION OF THE F
EFFECTIVE FLOW FACTOR')
WRITE(6,140) RUM(1)
140 FORMAT(1H),100X,'RUM #',2X,A8,2X,'PAGE 3',/)
WRITE(6,142)
142 FORMAT(1H,9X,'15',13X,'14',13X,'13',13X,'12',13X,'11',13X,'10',14
1X,'9',14X,'8',/)
FORM(1) = LEFT

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FORM(J0)=RIGHT
DO 200 I = 1.5
DO 190 M = 1.8
DO 180 J=1.8
IF (RESULT3(I,J,M).EQ.0.0) GO TO 170
FORM(J+1) = FSPEC
GO TO 180
170 FORM(J+1) = ASPEC
RESULT3(I,J,M) = BLANKS
180 CONTINUE
WRITE(6,FORM)(RESULT3(I,J,M),J=1.8)
WRITE(6,101) COLUMN(M)
191 FORMAT(1H+.122X.A8)
IF(M.NE.4.0) GO TO 190
WRITE(6,102) COLUMN(I)
192 FORMAT(1H+.126X.A4)
190 CONTINUE
200 CONTINUE
WRITE(6,210) RUN(I)
210 FORMAT(1H1.100X.10UN #1.2X.A8.2X.1PAGE 41.1)
WRITE(6,212)
212 FORMAT(1H.8X.115.13X.14.13X.13.13X.12.13X.11.13X.10.14
1X.10.14X.11.11)
FORM(I)=LEFT
FORM(J0)=RIGHT
DO 300 I = 6.8
DO 285 M = 1.8
DO 270 J = 1.8
IF (RESULT3(I,J,M).EQ.0.0) GO TO 255
FORM(J+1) = FSPEC
GO TO 270
255 FORM(J+1) = ASPEC
RESULT3(I,J,M) = BLANKS
270 CONTINUE
WRITE(6,FORM)(RESULT3(I,J,M),J=1.8)
WRITE(6,286) COLUMN(M)
286 FORMAT(1H+.122X.A8)
IF(M.NE.4.0) GO TO 285
WRITE(6,288) COLUMN(I)
288 FORMAT(1H+.126X.A4)
285 CONTINUE
300 CONTINUE
WRITE(6,400)
400 FORMAT(//.1X.1TABLE # 2 THE SQUARE OF THE STANDARD DEVIATION IS MA
1DE UP OF: .//1X.11* CONTRIBUTION OF NORMALIZATION FACTOR
2.//1X.12* CONTRIBUTION OF POWER.//1X.13* CONTRIBUTION OF OUTLET TEM
PERATURE.//1X.14* CONTRIBUTION OF INLET TEMPERATURE.//1X.15* TOTAL
4 CONTRIBUTION OF POWER.//1X.16* TOTAL CONTRIBUTION OF OUTLET TEMPE
RATURE.//1X.17* TOTAL CONTRIBUTION OF INLET TEMPERATURE)
DO 450 I=1.8
DO 450 J=1.8
DO 450 N=1.8
RESULT1(I,J,N)=0.0
450 CONTINUE
DO 460 I=1.8
DO 460 J=1.8
IF(TOUT(I,J).EQ.0.0) GO TO 460
N=1
RESULT1(I,J,N)=TOUT(I,J)
N=2

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RESULT(I,J,N)=HOUT(I,J)
N=3
RESULT(I,J,N)=X(I,J)
N=4
RESULT(I,J,N)=O(I,J)
N=5
RESULT(I,J,N)=SIPPO(I,J)
N=6
RESULT(I,J,N)=SITOUT(I,J)
N=7
RESULT(I,J,N)=SITIN(I,J)
460 CONTINUE
WRITE(6,500) RIIN(1)
500 FORMAT(1H).25X,'EFFECTIVE FLOW FACTOR DISTRIBUTION #',A8.27X,'PAGE
IF 51.//1H'.10X,'THESE VALUES ARE THE INPUTS USED FOR THE COMPUTATION'.
2/1H'.8X.'.15'.13X.'.14'.13X.'.13'.13X.'.12'.13X.'.11'.13X.'.10'.14X.'.9'.
3)4X.'.8'.//)
FORMA(1)=LEFTA
FORMA(10)=RIGHTA
DO 510 I=1.5
DO 505 M=1.8
DO 504 J=1.8
IF(RESULT(I,J,M).EQ.0.0) GO TO 503
FORMA(J+1)=FSPECA
GO TO 504
503 FORMA(J+1)=ASPECA
RESULT(I,J,M)=RLANKA
504 CONTINUE
WRITE(6,FORMA) (RESULT(I,J,M),J=1.8)
WRITE(6,507) COLUMN(M)
507 FORMAT(1H+.122X.A8)
IF(M.NE.4) GO TO 505
WRITE(6,506) COLUMN(I)
506 FORMAT(1H+.126X.A4)
505 CONTINUE
510 CONTINUE
WRITE(6,520) RIIN(1)
520 FORMAT(1H).100X,'RIIN #',2X.A8.2X,'PAGE 6',/
WRITE(6,212)
FORMA(1)=LEFTA
FORMA(10)=RIGHTA
DO 610 I=6.8
DO 605 M=1.8
DO 604 J=1.8
IF(RESULT(I,J,M).EQ.0.0) GO TO 603
FORMA(J+1)=FSPECA
GO TO 604
603 FORMA(J+1)=ASPECA
RESULT(I,J,M)=RLANKA
604 CONTINUE
WRITE(6,FORMA) (RESULT(I,J,M),J=1.8)
WRITE(6,607) COLUMN(M)
607 FORMAT(1H+.122X.A8)
IF(M.NE.4) GO TO 605
WRITE(6,606) COLUMN(I)
606 FORMAT(1H+.126X.A4)
605 CONTINUE
610 CONTINUE
WRITE(6,530)
530 FORMAT(1H'.10X,'THE ABOVE DATA ARE: 1* OUTLET TEMPERATURE (DEG. F.

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1) 1./14 .20X.12* OUTLET ENTHALPY (BTU/LR) 1./14 .20X.13* ENTHALPY D
2) IFFERENCE ACROSS THE FUEL ASSEMBLY (BTU/LR) 1./14 .20X.14* RELATIVE
3) POWER OF THE FUEL ASSEMBLY 1./14 .20X.15* RELATIVE POWER UNCERTAIN
4) TY 1./14 .20X.16* OUTLET TEMPERATURE UNCERTAINTY (DEG. F) 1./14 .20
5) X.17* INLET TEMPERATURE UNCERTAINTY (DEG. F) 1./14 *NOTE: THE
6) UNCERTAINTIES ARE RELATED TO A ONE SIGMA CONFIDENCE LEVEL. 1./)
WRITE(6,535) TIN , HIN(1)
535 FORMAT(14 .1INLET TEMPERATURE =1.F6.2,1DEG. F.,10X,1INLET ENTHALPY
1Y=1.F10.5,1BTU/LR)
STOP
END

```

INPUT FOR FLOFA 4  
\*\*\*\*\*

NRQ

1917.5

3R 522.3

( 1 1) 1R.7Y. F15.5.  
( 1 1) 1R.7Y. F15.10.

0 0 N M L K J H  
1\* 2\* 3\* 4\* 5\* 6\* 7\*  
1\* 2\* 3\* 4\*

1	R	0.7690	573.8	0.04001	2.14	0.1
2	5	0.7366	571.6	0.05506	2.14	0.1
2	6	1.0118	575.7	0.05539	2.14	0.1
2	7	1.2005	588.2	0.03157	2.14	0.1
3	4	0.7895	572.2	0.04863	2.14	0.1
3	5	0.9347	578.5	0.03029	2.14	0.1
3	7	1.0156	576.4	0.02360	2.14	0.1
3	8	1.0228	574.3	0.03057	2.14	0.1
4	4	1.0610	582.7	0.03095	2.14	0.1
4	5	1.1784	583.7	0.02309	2.14	0.1
4	6	1.1570	577.8	0.02850	2.14	0.1
4	7	1.1570	583.0	0.02331	2.14	0.1
5	2	0.7085	574.8	0.04955	2.14	0.1
5	3	1.2356	584.7	0.03087	2.14	0.1
5	4	1.1817	586.2	0.02382	2.14	0.1
5	5	0.9401	575.1	0.02143	2.14	0.1
5	6	0.9730	575.3	0.02336	2.14	0.1
5	7	0.9850	576.6	0.02332	2.14	0.1
5	8	1.0883	578.7	0.04010	2.14	0.1
6	2	0.9782	573.5	0.04748	2.14	0.1
6	3	0.9292	575.3	0.02993	2.14	0.1
6	4	1.1633	573.4	0.02341	2.14	0.1
6	5	0.9801	575.7	0.02327	2.14	0.1
6	6	1.1025	574.5	0.02314	2.14	0.1
7	1	0.731	566.4	0.05745	2.14	0.1
7	2	1.238	586.4	0.02655	2.14	0.1
7	4	1.1709	583.5	0.02331	2.14	0.1
7	6	1.1355	581.1	0.02332	2.14	0.1
7	7	0.9258	572.2	0.02311	2.14	0.1
7	8	1.0256	576.0	0.04029	2.14	0.1
8	1	0.7956	568.4	0.05745	2.14	0.1
8	2	0.9572	572.5	0.03050	2.14	0.1
8	3	1.1094	572.6	0.02920	2.14	0.1
8	4	0.9769	575.0	0.02891	2.14	0.1
8	5	1.1263	580.9	0.02841	2.14	0.1
8	6	0.8549	570.3	0.02836	2.14	0.1
8	7	1.0323	577.5	0.02855	2.14	0.1
8	8	0.9026	569.3	0.04002	2.14	0.1

497.3	500.0	1.154
498.0	510.0	1.170
510.7	520.0	1.185
522.6	530.0	1.205
534.8	540.0	1.230
547.2	550.0	1.250
559.8	560.0	1.280
572.8	570.0	1.315
586.1	580.0	1.350
599.8	590.0	1.395
614.0	600.0	1.450

1



EFF = CONSTANT \* RELATIVE POWER / ENTHALPY DIFFERENCE ACROSS THE FUEL ASSEMBLY

RESULTS: SUM OF THE RATIOS	=	0.5593390775
NORMALIZATION FACTOR	=	67.9373237565
SUM OF THE STD. SQUARE	=	0.0000242401
CONTRIBUTION OF POWER	=	0.0000092882
CONTRIBUTION OF T. OUT	=	0.0000149260
CONTRIBUTION OF T. INL	=	0.0000000258

THERMAL POWER = 1813.5 MWTH

15	14	13	12	11	10	9	8	
							0.8110250705	1*
							0.0023863109	2* R
							0.0488498808	3*
							6.0232269748	4*
				0.8138204400	1.0268132197	0.9721296014		1*
				0.0034598650	0.0052388991	0.0021991437		2* P
				0.0588206165	0.0723802357	0.0468950283		3*
				7.2277143715	7.0490171237	4.8239481867		4*
			0.8610913180		0.8985823359	1.0165325379	1.0676730085	1*
			0.0033440438		0.0021440007	0.0024951034	0.0033366103	2* N
			0.0578277677		0.0463033548	0.0499510102	0.0577633991	3*
			6.7156300999		5.1529340077	4.9138624085	5.4102144251	4*
			0.9447453458	1.0299148654	1.1280185150	1.0076594568		1*
			0.0022262796	0.0021510311	0.0033001689	0.0020612260		2* M
			0.0471834678	0.0463792093	0.0574470969	0.0454007271		3*
			4.5943054015	4.5032080673	5.0927441494	4.5055625477		4*
	0.7321032729	1.0612035801	0.9892127048	0.9748025205	0.9953474676	0.9820557946	1.0423237015	1*
	0.0023658542	0.0027118316	0.0019243045	0.0022791074	0.0024490035	0.0023044588	0.0036233642	2* L
	0.048600468	0.0520752489	0.0438668658	0.0477399977	0.0494874073	0.0480004792	0.0601943868	3*
	6.6438777992	4.9071856033	4.4345261215	4.8973999475	4.9718725280	4.8881926563	5.7750185210	4*
	1.0380975707	0.9505414870	1.2370895073	0.9946428509	1.1461850315			1*
	0.0046367430	0.0025498197	0.0039845113	0.0024162075	0.0033032885			2* K
	0.0680936341	0.0504557390	0.0631229851	0.0491549341	0.0574742424			3*
	6.5595269656	5.3123130023	5.1025382027	4.9419682729	5.0143947771			4*
0.9081832318	1.0328548932		1.0348737161		1.0409972826	1.0097509084	1.0346512517	1*
0.0049315929	0.0022368934		0.0021914741		0.0023314738	0.0027316673	0.0037525272	2* J
0.0702253011	0.0472958078		0.0468131825		0.0482853377	0.0522653543	0.0612578743	3*
7.7325036057	4.5791338274		4.5235647350		4.6383730775	5.1760641069	5.9206301795	4*
0.5435772355	1.0373533419	1.2970826016	0.9874716795	1.0354796978	0.9718486342	1.0114468158	0.9328263057	1*
0.0051407295	0.0032905496	0.0049920206	0.0026562625	0.0025991425	0.0029330497	0.0026682953	0.0034729339	2* H
0.0716588809	0.0573037125	0.0706542230	0.0515289413	0.0509817859	0.0541576379	0.0516555448	0.0589316039	3*
7.5986234303	5.5297756505	5.4471652678	5.2192829759	4.9234944955	5.5726412564	5.1070945126	6.3175323774	4*

TABLE # 1: THE FOLLOWING VALUES INCLUDED ARE:

- 1\* EFFECTIVE FLOW FACTOR NORMALIZED TO 1 OVER THE ASSEMBLIES WITH OUTLET THERMOCOUPLES
- 2\* SQUARE OF THE STANDARD DEVIATION OF THE EFFECTIVE FLOW FACTOR
- 3\* STANDARD DEVIATION OF THE EFFECTIVE FLOW FACTOR
- 4\* RELATIVE STANDARD DEVIATION OF THE EFFECTIVE FLOW FACTOR

15 14 13 12 11 10 9 8

2.1350367974 1\*  
 44.1122181590 2\*  
 53.6587677974 3\*  
 0.0939772461 4\* R  
 44.9303139539 5\*  
 54.9734342825 6\*  
 0.0022745175 7\*

1.4828265038 1.5589977208 3.3266508282 1\*  
 58.0201949056 61.7340315979 42.8187350913 2\*  
 40.4253501381 36.6434316625 53.7662379553 3\*  
 0.0716284525 0.0635390187 0.0863761252 4\* P  
 58.5883790834 62.3314027913 44.0941956588 5\*  
 41.3384127654 37.603973438 55.8158821064 6\*  
 0.0015796987 0.0016608462 0.0035461097 7\*

1.7175406020 2.9170136677 3.2075655496 2.6461190472 1\*  
 52.4242204108 34.5424740505 23.0576995296 31.9165927093 2\*  
 45.7773847777 62.4338253554 73.6075679893 65.3231839549 3\*  
 0.0808542095 0.1066869264 0.1271669325 0.1141052887 4\* N  
 53.0823415007 35.6602049571 24.2867630709 32.9305227969 5\*  
 46.8349745433 64.230005360 75.5826528826 66.9525529270 6\*  
 0.0018297465 0.0031075805 0.0034171140 0.0028189874 7\*

3.1053419930 3.8193760798 2.9863240789 3.8153957287 1\*  
 38.3925688948 26.2818976094 31.5051590228 26.7571938825 2\*  
 58.4048203551 69.7822717535 65.3963592860 69.3124849638 3\*  
 0.0972687170 0.1154545573 0.1121576123 0.1145254250 4\* M  
 39.5824627782 27.7453925308 32.6494480458 28.2191636271 5\*  
 60.3169602925 72.1350840182 67.2352129229 71.6622462945 6\*  
 0.0033082122 0.0040688937 0.0031814189 0.0040646534 7\*

1.7548735080 3.2166140793 3.9386732865 3.2290937192 3.1331288980 3.2413390764 2.3225730359 1\*  
 55.6095735665 39.5625481473 28.8436290207 19.1395774292 22.0668513001 22.7508688258 48.2030539591 2\*  
 42.5614027342 57.1255427941 67.1084741327 77.4961282542 74.6702709619 73.8802875135 49.3900630574 3\*  
 0.0741501914 0.0938549793 0.1092235601 0.1348005975 0.1297488401 0.1275045843 0.0843099475 4\* L  
 56.2819997483 40.7954788724 30.3528356207 20.3772900582 23.2673924707 23.9928735872 49.0930092219 5\*  
 43.6415805439 59.1071993947 65.5337446345 79.4844692957 76.5995209747 75.8761687346 50.8202065252 6\*  
 0.0018695184 0.0034267536 0.0041959846 0.0034430406 0.0033378144 0.0034530979 0.0024743054 7\*

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15	14	13	12	11	10	9	8	
	1.8302644069	2.7445517899	2.9746878471	3.1711659471	3.0801980720			1*
	52.3810433939	31.7322811403	21.0407228525	22.1629805416	21.2873589448			2*
	45.7384596795	65.4055055485	75.8514635852	74.5366084394	75.5006985163			3*
	0.0802325197	0.1136571214	0.1331257113	0.1292450719	0.1317444669			4* K
	53.1718622966	32.7835287189	22.1805531456	23.3780966133	22.4676182702			5*
	46.8465873090	67.0594903080	77.6831521206	76.4892799784	77.3973558373			6*
	0.0019178747	0.0029238518	0.0031690225	0.0033783364	0.0032814257			7*
	1.2955150954	3.6939179716	3.7850804925		3.5999785074	2.8907522062	2.2097050201	1*
	55.1872779024	33.6072307058	26.5445945322		25.2681490175	19.9263239279	46.2961915702	2*
	43.4380742715	62.5971032824	69.5550962118		71.0123466665	77.0468400468	51.4051079760	3*
	0.0791327307	0.1017480398	0.1152287635		0.1195258086	0.1360838190	0.0889954337	4* J
	55.6836887619	35.0226530363	27.9945481926		26.6475759586	21.0339920612	47.1428984687	5*
	44.2357983570	64.8716636844	71.8657906863		73.2290630697	78.8268445163	52.7657520339	6*
	0.0013801504	0.0039352395	0.0340323576		0.0038351630	0.0030796034	0.0023540638	7*
	1.3415861732	2.5329028586	2.6102885822	2.8432522233	3.1952178363	2.4940138955	1.9406911422	1*
	57.1498466029	30.5910171456	28.7257023396	30.6710045270	33.2858283011	25.8897437067	31.2406944571	2*
	41.4338904746	66.7583551729	68.5432006668	66.3707781721	63.4120786600	71.4886963627	65.6769308555	3*
	0.0746707493	0.1177248229	0.1208084114	0.1149650776	0.1068752026	0.1275460351	0.1128152328	4* H
	57.6639158139	31.5615658406	29.7259034205	31.7604717860	34.5101604900	26.8453910673	32.3785596712	5*
	42.2599832055	68.3180109606	70.1505073509	68.1215341361	65.3795603478	73.0244059512	67.5054615369	6*
	0.0014292312	0.0026903760	0.0027808172	0.0030290003	0.0034039596	0.0026569464	0.0031635591	7*

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TABLE # 2 THE SQUARE OF THE STANDARD DEVIATION IS MADE UP OF:

- 1\* CONTRIBUTION OF NORMALIZATION FACTOR
- 2\* CONTRIBUTION OF POWER
- 3\* CONTRIBUTION OF OUTLET TEMPERATURE
- 4\* CONTRIBUTION OF INLET TEMPERATURE
- 5\* TOTAL CONTRIBUTION OF POWER
- 6\* TOTAL CONTRIBUTION OF OUTLET TEMPERATURE
- 7\* TOTAL CONTRIBUTION OF INLET TEMPERATURE

THESE VALUES ARE THE INPLTS USED FOR THE COMPUTATION

15	14	13	12	11	10	9	8	
								573.80000 1*
								577.85400 2*
								64.41700 3*
								0.76900 4* R
								0.04001 5*
								2.14000 6*
								0.10000 7*
				571.60000	575.70000	588.20000		1*
				574.92800	580.38100	597.33400		2*
				61.49100	66.94400	83.89700		3*
				0.73660	1.01180	1.20050		4* P
				0.05506	0.05539	0.03157		5*
				2.14000	2.14000	2.14000		6*
				0.10000	0.10000	0.10000		7*
			572.20000		578.50000	576.40000	574.30000	1*
			575.72600		584.10500	581.31200	578.51900	2*
			62.28900		70.66800	67.87500	65.08200	3*
			0.78950		0.93470	1.01560	1.02280	4* N
			0.04863		0.03029	0.02360	0.03057	5*
			2.14000		2.14000	2.14000	2.14000	6*
			0.10000		0.10000	0.10000	0.10000	7*
			582.70000	583.70000	577.80000	583.90000		1*
			585.79900	591.16900	583.17400	591.44300		2*
			76.36200	77.73200	65.73700	78.00600		3*
			1.06190	1.17840	1.15790	1.15700		4* M
			0.03095	0.02309	0.02859	0.02331		5*
			2.14000	2.14000	2.14000	2.14000		6*
			0.10000	0.10000	0.10000	0.10000		7*
574.80000	584.70000	586.20000	575.10000	575.30000	576.60000	578.70000		1*
579.18400	592.53400	594.59400	575.58300	575.84900	581.57800	584.37100		2*
65.74700	79.10200	81.15700	66.14600	66.41200	68.14100	70.93400		3*
0.70850	1.23560	1.18170	0.94910	0.97300	0.98500	1.08830		4* L
0.04955	0.03077	0.02382	0.02143	0.02336	0.02332	0.04010		5*
2.14000	2.14000	2.14000	2.14000	2.14000	2.14000	2.14000		6*
0.10000	0.10000	0.10000	0.10000	0.10000	0.10000	0.10000		7*

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15	14	13	12	11	10	9	8	
	573.50000	575.30300	573.40000	575.70000	574.50000			1*
	577.45500	575.84500	577.32200	580.38100	578.78500			2*
	64.01800	66.41200	63.98500	66.94400	65.34800			3*
	0.97820	0.92920	1.16330	0.98010	1.10250			4* K
	0.04748	0.02593	0.02341	0.02327	0.02314			5*
	2.14000	2.14000	2.14000	2.14000	2.14000			6*
	0.10000	0.10000	0.10000	0.10000	0.10000			7*
566.40000	586.40000		583.50000		581.10000	572.20000	576.00000	1*
568.12000	594.86800		590.89500		587.60700	575.72600	580.78000	2*
54.68300	81.43100		77.45800		74.17000	62.28900	67.34300	3*
0.73100	1.23800		1.17990		1.13650	0.92580	1.02560	4* J
0.05745	0.02655		0.02331		0.02332	0.02311	0.04029	5*
2.14000	2.14000		2.14000		2.14000	2.14000	2.14000	6*
0.10000	0.10000		0.10000		0.10000	0.10000	0.10000	7*
568.40000	572.50000	572.60000	575.90000	580.90000	570.30000	577.50000	569.30000	1*
570.72000	576.12500	576.25800	580.64700	587.33300	573.19900	582.77500	571.85000	2*
57.28300	62.68800	62.82100	67.21000	73.89600	59.76100	69.33800	58.45300	3*
0.79560	0.95720	1.15940	0.97690	1.12630	0.85490	1.03230	0.80260	4* H
0.05745	0.03059	0.02920	0.02891	0.02841	0.02836	0.02855	0.04002	5*
2.14000	2.14000	2.14000	2.14000	2.14000	2.14000	2.14000	2.14000	6*
0.10000	0.10000	0.10000	0.10000	0.10000	0.10000	0.10000	0.10000	7*

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THE ABOVE DATA ARE: 1\* OUTLET TEMPERATURE (DEG. F.)  
 2\* OUTLET ENTHALPY (BTU/LB)  
 3\* ENTHALPY DIFFERENCE ACROSS THE FUEL ASSEMBLY (BTU/LB)  
 4\* RELATIVE POWER OF THE FUEL ASSEMBLY  
 5\* RELATIVE POWER UNCERTAINTY  
 6\* OUTLET TEMPERATURE UNCERTAINTY (DEG. F.)  
 7\* INLET TEMPERATURE UNCERTAINTY (DEG. F.)

NOTE: THE UNCERTAINTIES ARE RELATED TO A ONE SIGMA CONFIDENCE LEVEL.

INLET TEMPERATURE = 522.30 DEG. F. INLET ENTHALPY = 513.43700 BTU/LB

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C      PROGRAM VARY
C*****
REAL *8 LEFT, RIGHT, ASPEC, FSPEC, BLANK, FORM
REAL FQNO, FDHNO, FQN, FDHN
INTEGER *2 AM, AN
DIMENSION FQNO(204), FDHNO(204), FQN(204), FDHN(204), CASE(10),
IAM(204), AN(204), COLUM(15), TITLEA(3,6), TITLEB(3,6)
DIMENSION OUT(46,16), GRAPH(46,32), OUT1(24,16)
COMMON LEFT, RIGHT, ASPEC, FSPEC, BLANK, FORM(18)
READ(5,1) LEFT, RIGHT, ASPEC, FSPEC, BLANK
1  FORMAT(5A7)
   READ(5,2) (AM(I), AN(I), I=1,204)
2  FORMAT(36I2)
   READ(5,3) (FDHNO(I), FQNO(I), I=1,204)
3  FORMAT(12F6.4)
   READ(5,4) (COLUM(M), M=1,15)
4  FORMAT(15A2)
   READ(5,5) ((GRAPH(IY,IX), IX=1,15), IY=1,23)
5  FORMAT(15A4)
   READ(5,51) ((GRAPH(IY,IX), IX=16,32), IY=1,23)
51 FORMAT(17A4)
   READ(5,52) ((TITLEA(K,L), L=1,6), K=1,3)
52 FORMAT(6A4)
   READ(5,52) ((TITLEB(K,L), L=1,6), K=1,3)
   DO 11 IB=24,46
   DO 11 IA =1,32
   IY=47 - IB
   GRAPH(IB,IA)=GRAPH(IY,IA)
11 CONTINUE
   M = 1
   DO 12 IB =2,44,3
   GRAPH(IB,1) =COLUM(M)
   M = M+1
12 CONTINUE
   READ(5,53) ((GRAPH(IY,IX), IX=24,26), IY=2,5)
53 FORMAT(3A4)
   READ(5,54) ((GRAPH(IY,IX), IX=2,8), IY= 5, 9)
54 FORMAT(7A4)
   READ(5,6) LL
6  FORMAT(I5)
   DO 800 II=1,LL
   DO 16 IX=1,16
   DO 15 IY=1,46
   OUT(IY,IX)=0.0
15 CONTINUE
   DO 16 IY=1,24
   OUT1(IY,IX)=0.0
16 CONTINUE
   READ(5,7) CASE(II)
7  FORMAT(A3)
   READ(5,52) (GRAPH(2,IX), IX=27,32)
   READ(5,52) (GRAPH(5,IX), IX=27,32)
   READ(5,3) (FDHN(I), FQN(I), I=1,204)
   DO 20 I=1,157
   IX=AM(I)
   IY=AN(I)
   IY1=IY+1
   OUT (IY,IX)=((FQN(I)/FQNO(I))-1.)*200.
   OUT (IY1,IX)=((FDHN(I)/FDHNO(I))-1.)*200.

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20 CONTINUE
DO 30 I=158,204
  IX=AM(I)
  IC=AN(I)
  IC1=IC+1
  OUT1(IC,IX)=((FQN(I)/FQNO(I))-1.)*200.
  OUT1(IC1,IX)=((FDHN(I)/FDHNO(I))-1.)*200.
30 CONTINUE
DO 150 IY=38,40
DO 150 IX=27,32
  IK=IY-37
  IL=IX-26
  GRAPH(IY,IX)=TITLEA(IK,IL)
150 CONTINUE
  WRITE(6,8) CASE(II)
  8 FORMAT(1H1,' VARIATION OF FQN AND FDHN FOR A VARIATION OF 10 E-03
  1IN CASE #',2X,A3,/)
  WRITE(6,9)
  9 FORMAT(1H ,9X,'15',5X,'14',5X,'13',5X,'12',5X,'11',5X,'10',6X,'9',
  16X,'8',6X,'7',6X,'6',6X,'5',6X,'4',6X,'3',6X,'2',6X,'1',/)
DO 500 IA=1,46
  CALL PRESEN(OUT,46,16,IA,J,16)
500 WRITE(6,200)(GRAPH(IA,IB),IB=1,32)
200 FORMAT(1H+,32A4)
  WRITE(6,8) CASE(II)
  WRITE(6,9)
DO 160 IY=38,40
DO 160 IX=27,32
  IK=IY-37
  IL=IX-26
  GRAPH(IY,IX)=TITLEB(IK,IL)
160 CONTINUE
DO 700 IA=1,24
  CALL PRESEN(OUT1,24,16,IA,J,16)
700 WRITE(6,200)(GRAPH(IA,IB),IB=1,32)
DO 400 IA=25,46
  WRITE(6,100)(GRAPH(IA,IB),IB=1,32)
100 FORMAT(1H ,32A4)
400 CONTINUE
800 CONTINUE
  STOP
  END
  SUBROUTINE PRESEN(ARRAY,IY1,IX1,I,J,ID)
  REAL *8 LEFT, RIGHT, ASPEC, FSPEC, BLANK, FORM
  DIMENSION ARRAY(IY1,IX1)
  COMMON LEFT, RIGHT, ASPEC, FSPEC, BLANK, FORM(18)
  FORM(1)=LEFT
  FORM(18)=RIGHT
  DO 170 J=1,ID
  IF(ARRAY(I,J).EQ.0.0) GO TO 155
  FORM(J+1)=FSPEC
  GO TO 170
155 FORM(J+1)=ASPEC
  ARRAY(I,J)=BLANK
170 CONTINUE
  WRITE(6,FORM)(ARRAY(I,J),J=1,ID)
  RETURN
  END

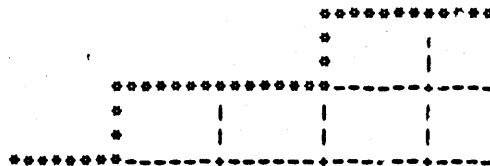
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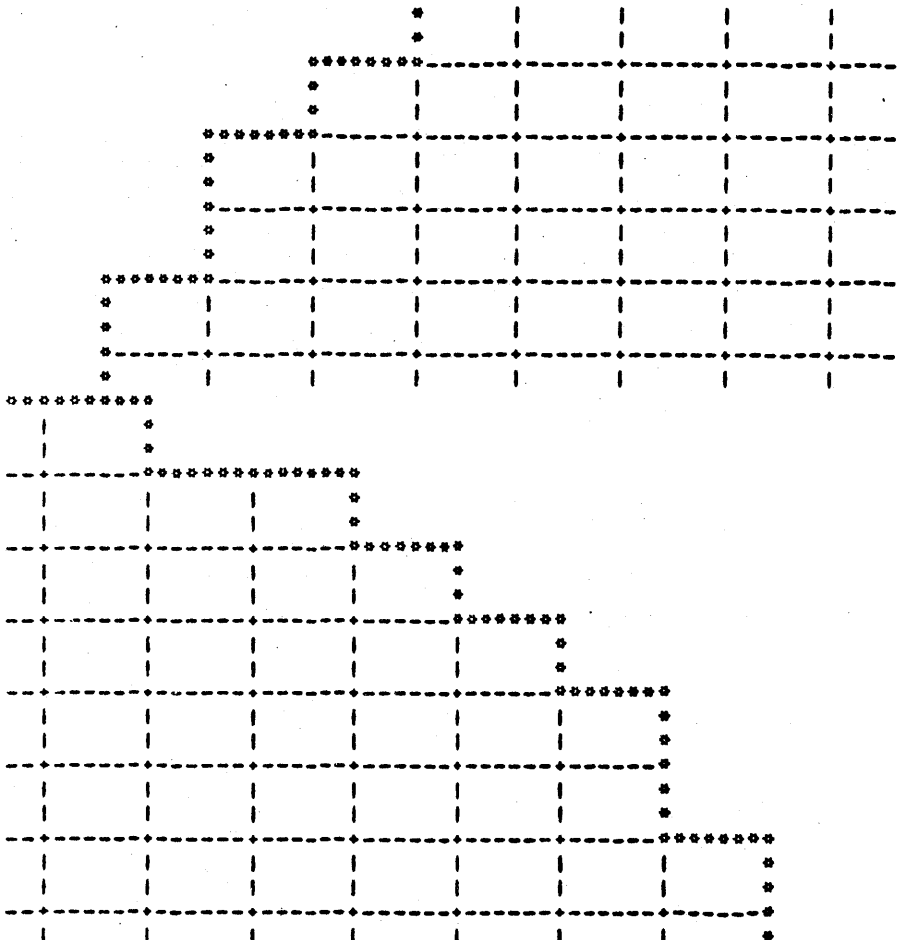


SAMPLE INPUT FOR VARY

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(      * )  A7.  F7.3.
 8 2 9 210 2 6 5 7 5 8 5 9 510 511 512 5 5 8 6 8 7 8 8 8 9 810 811 812 8
13 8 411 511 611 711 811 911101111111121113111411 314 414 514 614 714 814
914101411141214131414141514 317 417 517 617 717 817 9171017111712171317
14171517 220 320 420 520 620 720 820 9201020112012201320142015201620 223
323 423 523 623 723 823 9231023112312231323142315231623 226 326 426 526
626 726 826 9261026112612261326142615261626 329 429 529 629 729 829 929
102911291229132914291529 332 432 532 632 732 832 93210321132123213321432
1532 435 535 635 735 835 93510351135123513351435 538 638 738 838 9381038
113812381338 641 741 841 941104111411241 844 9441044 8 2 9 2 6 5 7 5 8 5
9 5 5 8 6 8 7 8 8 8 9 8 411 511 611 711 811 911 314 414 514 614 714 814
914 317 417 517 617 717 817 917 220 320 420 520 620 720 820 920 223 323
423 523 623 723 823 923
.6931 .8761 .7690 .9270 .6537 .7880 .7366 .93111.01181.27891.20051.4907
.87881.05931.15811.3960 .95431.1503 .6842 .8408 .7895 .97031.24241.5414
.93471.15591.01561.24651.02281.2383 .99951.2193 .91161.09891.20571.4817
.7895 .9703 .7986 .99741.06191.32381.17841.44631.15791.40331.15701.4116
.92811.14821.15401.41681.15061.41401.16791.43531.05221.2931 .7916 .9728
.7085 .87021.23561.52751.18171.4594 .94911.1622 .97301.1821 .98501.2022
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.93781.1235 .98331.1780 .7313 .93771.23821.53021.03561.25801.17991.4381
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.7935 .96661.21181.4762 .90461.07771.00261.19451.01901.21401.00261.1945
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1.11991.36291.29061.54841.04281.25001.17621.40791.07981.38451.04871.2809
1.31641.58351.03061.24531.24421.5040 .91091.09871.14161.3712 .8330 .9971
R P N M L K J H G F E D C B A
```





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*****
| ENTIRE ASSEMBLY |
*****
=====
| HOTTEST ROD ONLY |
=====
VARIATION OF

```

```

IN ASSEMBLY
VARIATION OF FON . . . . .
VARIATION OF FDHN. . . . .
*****
UNITS = 1.0 E-03 *
----- *
1

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008
DETECTORS READINGS
M12
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```

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.6916 .84251.21511.48021.16861.4236 .94331.1491 .97331.1856 .99341.2102  
1.10881.3210 .98181.1977 .96181.1734 .93221.13721.15491.40891.20091.4649  
.6835 .8338 .7945 .96781.05621.28661.17231.42801.15491.40681.16281.3854  
.94171.12191.16281.38541.14131.39231.15851.41331.04381.2733 .7852 .9579  
.7924 .96531.21021.4742 .90341.07631.00131.19291.01761.21241.00131.1929  
.90341.07631.19601.4590 .7831 .9554 .6867 .8365 .94561.12661.14771.3673  
.87091.03751.14771.3673 .94561.1266 .6786 .8279 .6478 .7718 .7621 .9079  
.6478 .77181.06321.34391.03221.24411.14901.45241.32791.67851.42071.7547  
.99721.21141.26691.58151.52451.8855 .99231.21771.12911.38721.13271.3770  
1.27021.58571.29231.60601.32571.62451.29601.57231.30111.5904 .97491.2035  
1.10551.35781.52571.88581.33801.65171.08101.32731.08831.32291.10191.3439  
1.20471.49721.28621.5797 .98691.21051.30161.59311.09801.33571.24311.4982  
1.27501.5329 .89781.07461.11561.43041.47591.81541.16771.41441.33041.6178  
1.11841.36101.28891.54631.04141.24841.17461.40601.07841.38261.04731.2792  
1.31461.58141.02931.24361.24261.5019 .90971.09721.14001.3693 .8319 .9957

VARIATION OF FCN AND FDMA FOR A VARIATION OF 10 E-03 IN CASE # CCB

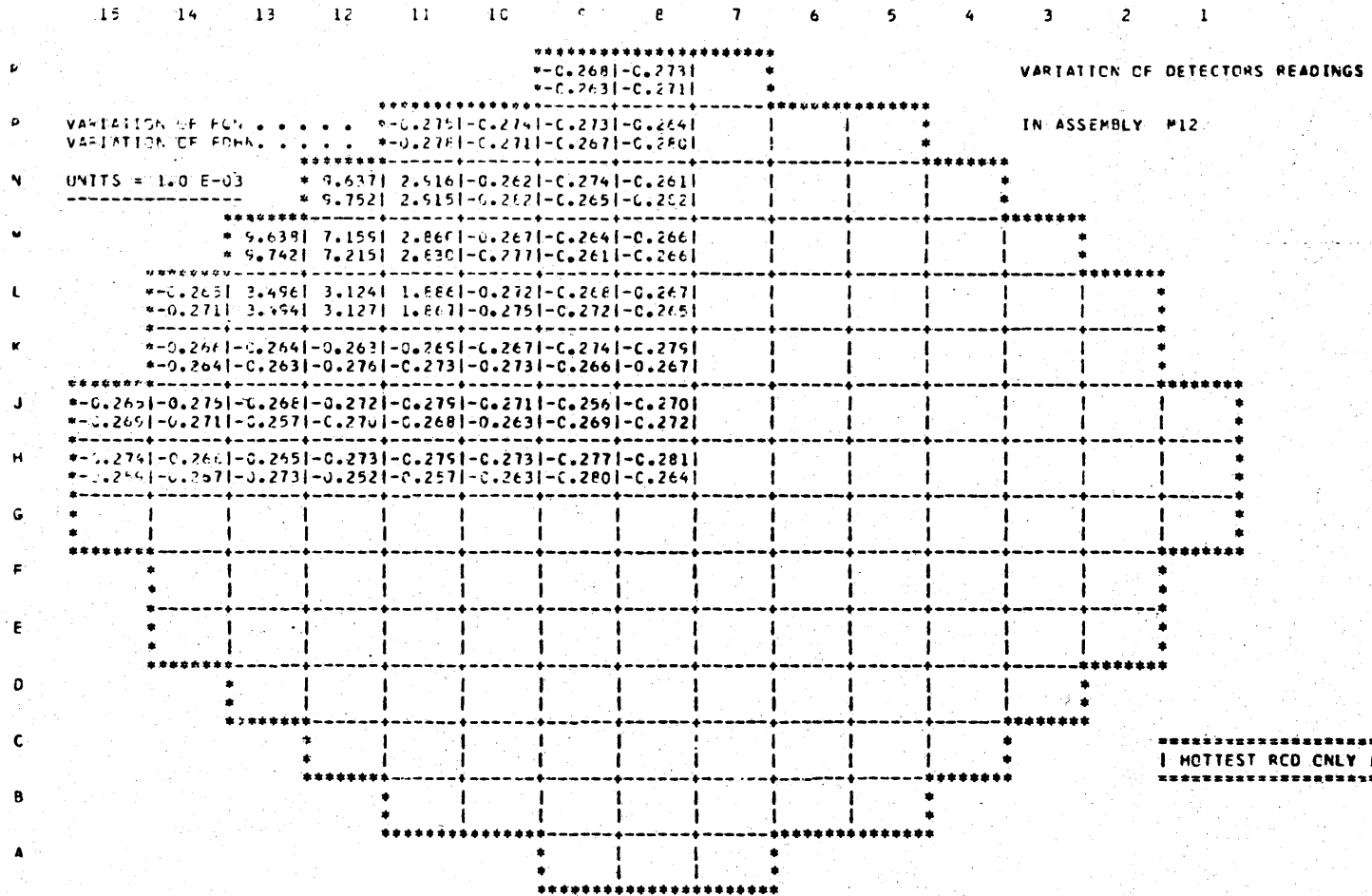
15 14 13 12 11 10 9 8 7 6 5 4 3 2 1

	15	14	13	12	11	10	9	8	7	6	5	4	3	2	1
	*****														
	*-0.251 -0.260 -0.275*														
	*-C.260 -0.260 -0.245*														
	*****														
P	*****														
VARIATION OF FCN . . . . .	*-0.259 -C.266 -C.268 -0.264 -0.272 -0.278 -J.262*														
VARIATION OF FDMA . . . . .	*-C.277 -C.277 -C.266 -0.273 -0.259 -0.272 -0.252*														
	*****														
N	*****														
UNITS = 1.0 E-03	*-0.289  2.594 -C.277 -C.273 -C.258 -0.279 -0.273 -C.270 -0.289*														
	*-0.279  2.594 -0.278 -C.276 -C.274 -C.260 -0.263 -0.265 -J.279*														
	*****														
M	*****														
	* 9.645  8.657  3.084 -C.271 -C.269 -0.279 -0.268 -0.269 -0.265 -0.263 -0.267*														
	* 9.742  8.735  3.372 -C.259 -C.259 -C.260 -C.277 -0.261 -0.257 -0.266 -0.278*														
	*****														
L	*****														
	*-0.253  3.627  3.454  0.585 -0.271 -C.266 -C.261 -C.263 -0.265 -0.277 -0.280 -0.269 -C.260*														
	*-0.254  3.626  3.466  0.565 -C.267 -C.264 -0.276 -C.266 -0.268 -0.277 -0.275 -0.264 -0.261*														
	*****														
K	*****														
	*-0.266 -C.281 -0.267 -0.268 -0.255 -C.268 -0.277 -C.263 -0.265 -0.265 -0.268 -0.267 -0.272*														
	*-0.266 -C.280 -0.275 -C.265 -C.272 -C.269 -C.260 -0.255 -0.253 -0.265 -0.277 -0.277 -0.264*														
	*****														
J	*****														
	*-J.277 -0.274 -C.270 -C.264 -0.263 -0.264 -0.271 -C.261 -0.252 -0.259 -0.257 -0.273 -0.272 -0.278 -0.271*														
	*-0.273 -0.279 -C.270 -0.271 -C.278 -C.264 -0.259 -C.273 -C.280 -0.265 -0.276 -0.278 -0.268 -0.267 -0.266*														
	*****														
H	*****														
	*-0.275 -0.270 -0.264 -0.271 -C.265 -0.252 -C.258 -C.271 -0.258 -0.267 -0.258 -0.270 -0.268 -0.275 -0.272*														
	*-0.277 -C.272 -C.267 -0.266 -0.266 -0.257 -C.271 -0.274 -0.270 -0.274 -0.258 -0.263 -0.271 -C.263 -0.271*														
	*****														
G	*****														
	*-0.277 -0.269 -C.265 -0.267 -0.276 -C.276 -C.269 -0.261 -0.252 -0.263 -0.277 -0.273 -0.272 -0.278 -0.271*														
	*-0.273 -C.270 -0.281 -C.272 -C.274 -C.261 -C.260 -C.273 -C.280 -C.267 -0.278 -0.278 -0.268 -0.267 -0.266*														
	*****														
F	*****														
	*-0.265 -0.261 -0.269 -0.266 -0.266 -0.266 -0.276 -0.267 -0.268 -0.269 -0.258 -0.267 -0.272*														
	*-0.264 -0.271 -0.259 -0.284 -C.270 -C.267 -C.262 -0.271 -0.273 -0.267 -0.262 -0.277 -0.264*														
	*****														
E	*****														
	*-0.234 -C.270 -C.267 -0.261 -0.269 -C.264 -0.257 -0.267 -0.255 -0.281 -0.269 -0.273 -0.287*														
	*-0.289 -0.279 -0.274 -0.275 -0.267 -0.281 -C.270 -C.264 -0.270 -0.275 -0.277 -0.266 -0.263*														
	*****														
D	*****														
	*-J.269 -C.264 -C.280 -C.270 -C.260 -0.267 -0.260 -0.273 -0.269 -0.267 -0.271*														
	*-0.277 -C.265 -C.272 -C.259 -C.275 -C.255 -C.275 -0.280 -0.276 -0.268 -0.254*														
	*****														
C	*****														
	*-0.265 -C.271 -C.260 -C.268 -0.263 -0.268 -0.260 -0.260 -0.251*														
	*-0.277 -C.264 -0.265 -C.259 -C.275 -0.259 -0.265 -0.267  0.281*														
	*****														
B	*****														
	*-0.263 -C.266  C.263 -0.270 -C.243 -J.266 -0.265*														
	*-0.262 -0.275 -C.261 -0.252 -0.261 -0.275 -0.265*														
	*****														
A	*****														
	*-C.259 -C.264 -0.255*														
	*-C.277 -C.262 -0.277*														
	*****														

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| ENTIRE ASSEMBLY |  
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202

VARIATION OF FOM WITH TEMPERATURE FOR A VARIATION OF 10 E-03 IN CASE # C08



203

\*DECK MAIN

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PROGRAM COHRA3C (INPUT,OUTPUT,TAPE5=INPUT,TAPE6=OUTPUT)
C THIS PROCEDURE CONTAINS THE COMMON AND TYPE STATEMENTS SHARED BY THEM
C MAJOR SUBROUTINES OF COHRA-IIIC.
COMMON KIJ, FIM, ABETA, BBETA, AFLUX, Z, THETA, PI, NAX, FLO,
1 GC, I3, I2, NCHANL, NK, IERROR, KDEBUG, NAXL, NGAPS, NGXL,
2 NAFAC, NODES, NSCHC, NARC, J1, J2, J3, J4, J5, J6, J7,
3 ATOTAL, DX, DT, GK, NV, NF, AV(7), AF(7), QAX, FSPLIT(30)
4 , ELEV, NDX, SL, FERROR, ITERAT, NRAMP, NVISW, NARAMP
COMMON PP(30), TT(30), VVF(30), VVG(30), MHF(30), MHG(30),
1 UUF(30), KKF(30), SSIGMA(30), NPROR, PREF, TF, VF, VG, HF, HG,
2 UF, KF, SIGMA, HFG, VFG, RHOF, RHOG
COMMON V(30), VP(30), VISC(30), VISCW(30), HFILM(30), CON(30),
1 CP(30), FSP(30), FMULT(30), U(30), UH(30), ALPHA(30), QUAL(30),
2 RHO(30,31), VPA(30), T(30), HINLET(30), FINLET(30)
COMMON COND(47), WP(47), GAP(47), FACTOR(47), JK(47),
1 JK(47), GAPN(47), LENGTH(47), USTAR(47), W(47,31)
COMMON A(30), AN(30), DHYD(30), DHYDN(30), DFDX(30),
1 DHDX(30), DPDY(30), OPRIM(30), PERIM(30),
2 HPERIM(30), NTYPE(30)
COMMON P(30,31), H(30,31), F(30,31), X(31)
COMMON WOLD(47,31), RHOOLD(30,31), FOLD(30,31), HOLD(30,31)
COMMON AXIAL(39), Y(39), IDAREA(30), IDGAP(47), AA( 4), BB( 4),
1 CC( 4), AFACT(10,10), NCH(10), AXL(10), GAPXL(10), GFACT( 9,10),
2 NGAP( 9), RX(30), XQUAL(30)
COMMON NGRID, NGRIDT, GRIDXL(10), IGRID(10), CD(30, 5),
1 FXFLOW(47, 5), NGTYPE, GRID, FDIV(47)
LOGICAL FDIV, GRID
REAL KIJ, LENGTH, KF, KKF
DIMENSION OUTPUT(10)
DIMENSION TEXT(17),LC(30,4),GAPS(30,4),AC(30),PW(30),
2 PH(30), DR(35), DC(30), DIST(30,4), IM( 9), JM( 9)
DIMENSION PRINT(12), PRINTC(30), SIGNAL(18)
DIMENSION TDUMY(10), PRINTN(10), PRINTR(35)
DIMENSION DATE(2), TIME(2)
DIMENSION TINLET(30)
DIMENSION YP(30), FP(30), YH(30), FH(30), YG(30), FG(30),
1 FQ(30), YQ(30)
DIMENSION CROSS(6), NWRAPS(30)
DIMENSION CHECOR(5)
COMMON /FUEL/ KFUEL( 3), KCLAD( 3), RFUEL( 3), RCLAD( 3),
1 CFUEL( 3), CCLAD( 3), TCLAD( 3), TFLUID,
2 FLUX(35,31), HGAP( 3), TROD(10,35,31), LR(35,6),
3 PWR(30,35), PHI(35,6), RADIAL(35), D(35),
4 POWER, NODESF, NPROD, DFUEL( 3), IDFUEL(35), HSURF
COMMON /BWRAP/ XCROSS(47,6),DUR(47),DIA,THICK,NWRAP(47),PITCH
COMMON /RSP/ SP(47,31)
COMMON/RCHF/ CHF(35,31), CCHANL(35,31), MCHFR(31), MCHFR(31),
1 MCHFR(31),NCHF
REAL MCHFR
REAL KFUEL, KCLAD
LOGICAL PRINT
INTEGER PRINTC
INTEGER PRINTN, PRINTR
INTEGER CCHANL
DATA CHECOR /4HRAW2,4HW-3 ,4H ,4H ,4H /
DATA H1,H2,H3,H4,H5 / 1H(, 1H,, 1H), 4H W(, 4H)WP( /
DATA H6, H7, H8 /1HW, 1HX, 2HT( /
DATA SIGNAL /4HMAIN,4HDIFF,4HVRT,4HMIX .

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14HSCHM,4HFORC,4HVOID,4HSPLT,4HAREA,4HCURV,4HPROP,
24HDCOM,4HSOLV,4HHEAT,4HTEMP,4HHCOL,4HGAUS,4HCIJ /
1 FORMAT(7I5)
2 FORMAT(2I5,17A4)
3 FORMAT(15H)INPUT FOR CASE           I6,5X,16A4,A2,
   19H  DATE 2A6,7H TIME 2A6           )
4 FORMAT (E5.2,F5.1,7F10.0)
5 FORMAT (12F5.3)
6 FORMAT (23HOHEAT FLUX DISTRIBUTION /23H X/L   RELATIVE FLUX /
   1(F7.3,F12.3))
7 FORMAT(I1,I4,3E5.2,4(I5,2E5.2))
8 FORMAT ( I5/(12F5.3))
9 FORMAT (6F10.0)
10 FORMAT(12E5.0)
11 FORMAT(I1,I4,2E5.2,6(I5,E5.2))
12 FORMAT(22HOSURCHANNEL INPUT DATA /
   1109H CHANNEL TYPE AREA WETTED HEATED HYDRAULIC (ADJ)MAIN3720
   2ACENT CHANNEL NO., SPACING, CENTROID DISTANCE) /
   3 55H NO. (SQ-IN) PERIM. PERIM. DIAMETER / MAIN3730
   4 25X, 30H (IN) (IN) (IN) / MAIN3740
   5 (I5,I7,4F10.6,4X,4(1H(I3,1H,F5.3,1H,F5.3,1H))) / MAIN3750
13 FORMAT(22HOFUID PROPERTY TABLE /
   1 60H P T VF VG HF HG MAIN3760
   1 30H VISC. KF SIGMA / MAIN3770
   1 (F8.1,F10.2,F8.5,F12.5,2F10.2,3F10.5)) MAIN3780
14 FORMAT(4E5.2,2I5,E5.2,I5,4E5.2) MAIN3790
15 FORMAT(15HOROD INPUT DATA / 96H ROD TYPE DIA RADIAL POWER MAIN3800
   1 FRACTION OF POWER TO ADJACENT CHANNELS (ADJ. CHANNEL NO.) / MAIN3810
   2 30H NO. NO. (IN) FACTOR / (2I5,F8.4,F9.4,F11.4,1H(I2,
   11H)F9.4,1H(I2,1H)F9.4,1H(I2,1H)F9.4,1H(I2,1H)F9.4,
   11H(I2,1H))) MAIN3820
17 FORMAT (36I2) MAIN3830
18 FORMAT (23HOCALCULATION PARAMETERS /
   2 28H CROSSFLOW RESISTANCE,KIJ F8.3/ MAIN3840
   4 28H MOMENTUM TURBULENT FACTORF8.4 / MAIN3850
   3 28H PARAMETER, (S/L) F8.3/ MAIN3860
   4 28H CHANNEL LENGTH F8.2,8H INCHES / MAIN3870
   4 28H CHANNEL ORIENTATION F8.1,8H DEGREES/ MAIN3880
   5 28H NUMBER OF AXIAL NODES I8/ MAIN3890
   6 28H NODE LENGTH F8.3,7H INCHES / MAIN3900
   7 28H NUMBER OF TIME STEPS I8/ MAIN3910
   8 28H TOTAL TRANSIENT TIME F8.3,8H SECONDS/ MAIN3920
   X 28H TIME STEP F8.4,8H SECONDS/ MAIN3930
   1 28H ALLOWABLE ITERATIONS I8/ MAIN3940
   2 28H FLOW CONVERGENCE FACTOR E10.5/) MAIN3950
19 FORMAT (50HO X/L AREA VARIATION FACTORS FOR SUBCHANNEL (I) /
   1 7X,10(3X,A1,I2,A1,1X)) MAIN4000
20 FORMAT (69HO X/L GAP SPACING VARIATION FACTORS FOR ADJACENT SUBMAIN4010
   1CHANNELS (I,J) / 7X,10(1X,A1,I2,A1,I2,A1)) MAIN4020
21 FORMAT (22HOOPERATING CONDITIONS /
   1 25H SYSTEM PRESSURE = ,F8.1,5H PSIA / MAIN4030
   2 25H INLET ENTHALPY = ,F8.1,7H BTU/LB / MAIN4040
   3 25H AVG. MASS VFLOCITY = ,F8.3,21H MILLION LB/(HR-SQFT) / MAIN4050
   2 25H INLFT TEMPERATURE = ,F8.1,10H DEGREES F / MAIN4060
   4 25H AVG. HEAT FLUX = ,F8.6,22H MILLION BTU/(HR-SQFT) ) MAIN4070
22 FORMAT (23HOFAILURE INTEGRATION IN,I4,I7H ITERATIONS AT X=
   1F8.4,2I10) MAIN4080
25 FORMAT(17H1CHANNEL RESULTS /
   1 5H CASEI5,5X17A4, 9H DATE 2A6,7H TIME 2A6/) MAIN4090

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28 FORMAT ( /29H FRICTION FACTOR CORRELATION ) MAIN4160
29 FORMAT ( 16H CHANNEL TYPE I3,11H FRICT = F5.3,6H*RE**(F5.3, MAIN4170
14H) * F6.4 ) MAIN4180
30 FORMAT(F7.1,10F10.5) MAIN4190
31 FORMAT (68H DIVERSION CROSSFLOW BETWEEN ADJACENT CHANNELS, W(I,J), MAIN4200
1 (LB/SEC-FT). MAIN4210
1 // 5H CASE IS , 5X, 17A4, MAIN4220
29H DATE 2A6,7H TIME 2A6 /// MAIN4230
3 5X,A1,2X,10(2X,A1,A1,I2,A1,I2,A1)) MAIN4240
32 FORMAT(31H SUBCOOLED MIXING, BETA = F6.4) MAIN4250
33 FORMAT(31H SUBCOOLED MIXING, BETA = F6.4,6H*RE**(F6.4,1H)) MAIN4260
34 FORMAT(31H SUBCOOLED MIXING, BETA = F6.4,12H*(D/S)*RE**(F6.4, MAIN4270
1 1H)) MAIN4280
35 FORMAT(20H MIXING CORRELATIONS ) MAIN4290
36 FORMAT(54H BOILING MIXING, BETA IS ASSUMED SAME AS SUBCOOLED) MAIN4300
37 FORMAT(55H BOILING MIXING, BETA IS A FUNCTION OF STEAM QUALITY/ MAIN4310
1 25H X BETA(X) / (F12.3,F13.6)) MAIN4320
38 FORMAT (F6.3,10F8.3) MAIN4330
39 FORMAT(31H SUBCOOLED MIXING, BETA = F6.4,12H*(D/L)*RE**(F6.4, MAIN4340
1 1H)) MAIN4350
40 FORMAT( F7.3,F10.3,2F10.2,4F10.4) MAIN4360
41 FORMAT (I5,7E10.5) MAIN4370
42 FORMAT(8E10.5) MAIN4380
43 FORMAT(2I5,6F5.4) MAIN4390
44 FORMAT( / 28H TWO-PHASE FLOW CORRELATIONS ) MAIN4400
45 FORMAT( 33H NO SUBCOOLED VOID CORRELATION ) MAIN4410
46 FORMAT( 35H LEVY SUBCOOLED VOID CORRELATION ) MAIN4420
47 FORMAT( 31H HOMOGENEOUS BULK VOID MODEL ) MAIN4430
48 FORMAT( 41H MODIFIED ARMAND BULK VOID CORRELATION ) MAIN4440
49 FORMAT( 50H HOMOGENEOUS BULK VOID MODEL WITH SLIP RATIO OF, MAIN4450
1 F6.2 ) MAIN4460
50 FORMAT(20I5) MAIN4470
51 FORMAT (8E12.3) MAIN4480
52 FORMAT (I5,6E12.6) MAIN4490
53 FORMAT (I5,3E12.6) MAIN4500
54 FORMAT(/// INPUT DATA ERROR, THIS RUN STOPPED, CHECK INPUT!) MAIN4510
55 FORMAT (10H ERROR IN A6,40H ** CALCULATION FOR THIS CASE STOPPED) MAIN4520
10. ) MAIN4530
56 FORMAT(10H ERROR IN A6,65H ** INITIAL CONDITION NOT ESTABLISHED) MAIN4540
1, CALCULATION STOPPED ) MAIN4550
57 FORMAT( 33H BULK VOID FRACTION GIVEN AS A 12,56H TERM POLYNOMIAL MAIN4560
FUNCTION OF QUALITY WITH COEFFICIENTS OF/ 10X,7E10.4) MAIN4570
58 FORMAT( 41H HOMOGENEOUS MODEL FRICTION MULTIPLIER ) MAIN4580
59 FORMAT( 30H ARMAND FRICTION MULTIPLIER ) MAIN4590
60 FORMAT( 34H FRICTION MULTIPLIER GIVEN AS A 12,57H TERM POLYNOMIAL MAIN4600
FUNCTION OF QUALITY WITH COEFFICIENTS OF/ 10X,7E10.4) MAIN4610
61 FORMAT(65H WALL VISCOSITY CORRECTION TO FRICTION FACTOR IS NOT MAIN4620
INCLUDED ) MAIN4630
62 FORMAT(65H WALL VISCOSITY CORRECTION TO FRICTION FACTOR IS INCL MAIN4640
LUDED ) MAIN4650
64 FORMAT(I5,10E5.2) MAIN4660
65 FORMAT(42H CONDUCTION MIXING, GEOMETRY FACTOR = F6.4) MAIN4670
66 FORMAT (6( E5.2,I5)) MAIN4680
67 FORMAT (I5,F5.2,I5,E5.2) MAIN4690
68 FORMAT(10I5) MAIN4700
69 FORMAT ( /62H WIRE WRAP SPACER DATA FOR FORCED DIVERSION CROSSFLOW MAIN4710
1 MIXING //20H WRAP PITCH = F6.1,7H INCHES / MAIN4720
2 20H WRAP THICKNESS = F6.4,7H INCHES / MAIN4730
3 20H PIN DIAMETER = F6.4,7H INCHES //) MAIN4740

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70 FORMAT (23H WRAP CROSSING DATA / MAIN4750
1 60H GAP SUBCHANNEL MIXING RELATIVE LOCATION MAIN4760
2 / 60H NO. PAIR NO. PARAMETER OF WRAP CROSSINGS MAIN4770
3 / (I10.4X,A1,I2,A1,I2,A1,F11.4,6F10.4)) MAIN4780
71 FORMAT ( / 12H SPACER DATA / 20H SPACER TYPE NO. ,1016 ) MAIN4790
72 FORMAT ( 21H LOCATION (X/L) ,10F6.3) MAIN4800
73 FORMAT (15H0 SPACER TYPE I2 / MAIN4810
1 62H CHANNEL DRAG CHANNEL DRAG CHANNEL DRAG CHANNEL DRAG MAIN4820
2/64H NO. COEFF. NO. COEFF. NO. COEFF. NO. COEFF. MAIN4830
3F. / (3X.4(I6.F9.3))) MAIN4840
74 FORMAT (46H INITIAL WRAP INVENTORY FOR EACH SUBCHANNEL / (1015)) MAIN4850
75 FORMAT ( // 14H ITERATIONS = I4) MAIN4860
76 FORMAT (43H0 FLOW DIVERSION FACTORS FOR SPACER TYPE I2/ MAIN4870
1 5X 46HGAP CHANNEL FRACTION GAP CHANNEL FRACTION / MAIN4880
25X 46HNO. PAIR DIVERTED NO. PAIR DIVERTED / MAIN4890
3 (2(5X,I3.1X,A1,I2,A1,I2,A1,F9.4))) MAIN4900
77 FORMAT (39H THERMAL PROPERTIES FOR FUEL MATERIAL MAIN4910
1 1R,18H RADIAL FUEL NODES / MAIN4920
1 37H FUEL PROPERTIES 25X15HCLAD PROPERTIES / MAIN4930
2 50H TYPE COND. SP. HEAT DENSITY DIA. MAIN4940
3 50H COND. SP. HEAT DENSITY THICK. GAP COND. / MAIN4950
4 49H NO. (B/HR-FT-F) (B/LB-F) (LB/FT3) (IN.) MAIN4960
5 52H(B/HR-FT-F) (B/LB-F) (LB/FT3) (IN.) (B/HR-FT2-F) MAIN4970
78 FORMAT (17.2X,F7.2,F11.4,F11.1,F9.4,2X,F7.2,F11.4,F11.1,F9.4,2X, MAIN4980
1 F9.2) MAIN4990
79 FORMAT ( 9F5.2) MAIN5000
80 FORMAT (8H TIME = F8.5. 9H SECONDS MAIN5010
1 20H DATA FOR CHANNEL I3/) MAIN5020
81 FORMAT (F6.1,F12.2,2F12.2,F10.2,2F9.3,F11.4,F12.4) MAIN5030
82 FORMAT ( * DISTANCE DELTA-P ENTHALPY TEMPERATURE DENSITY MAIN5040
1 EQUIL VOID FLOW MASS FLUX * (IN.) (PSI) (MAIN5050
18TU/LB) (DEG-F) (LB/CU-FT) QUALITY FRACTION (LB/SEC) (MLB/H) MAIN5060
1R-FT2) * ) MAIN5070
83 FORMAT (33H FORCING FUNCTION FOR PRESSURE / MAIN5080
1 23H TIME PRESSURE / MAIN5090
2 23H (SEC) FACTOR / (F10.4,F13.4)) MAIN5100
84 FORMAT (38H FORCING FUNCTION FOR INLET ENTHALPY/ MAIN5110
1 28H TIME INLET ENTHALPY / MAIN5120
2 23H (SEC) FACTOR / (F10.4,F13.4)) MAIN5130
85 FORMAT (38H FORCING FUNCTION FOR INLET FLOW / MAIN5140
1 28H TIME INLET FLOW / MAIN5150
2 23H (SEC) FACTOR / (F10.4,F13.4)) MAIN5160
86 FORMAT (38H FORCING FUNCTION FOR HEAT FLUX / MAIN5170
1 38H TIME HEAT FLUX / MAIN5180
2 23H (SEC) FACTOR / (F10.4,F13.4)) MAIN5190
87 FORMAT (30H UNIFORM INLET ENTHALPY ) MAIN5200
88 FORMAT (35H UNIFORM INLET TEMPERATURE ) MAIN5210
89 FORMAT (45H INDIVIDUAL SUBCHANNEL ENTHALPY SPECIFIED ) MAIN5220
90 FORMAT (50H INDIVIDUAL SUBCHANNEL TEMPERATURE SPECIFIED ) MAIN5230
91 FORMAT (35H UNIFORM INLET MASS VELOCITY ) MAIN5240
92 FORMAT (50H FLOWS SPLIT TO GIVE EQUAL PRESSURE GRADIENT ) MAIN5250
93 FORMAT (45H INDIVIDUAL SUBCHANNEL FLOWS SPECIFIED ) MAIN5260
94 FORMAT (5H1CASE15,5X1744.9H DATE 2A6,7H TIME 2A6// MAIN5270
1 8H TIME = F8.5,9H SECONDS MAIN5280
2 28H TEMPERATURE DATA FOR ROD I3. MAIN5290
3 12H FUEL TYPE I2// MAIN5300
4 * DISTANCE FLUX DNBR CHANNEL TEMPERATURE (F) * / MAIN5310
5 22H (IN.) (MBTU/HR-FT2) 13X,10(4X,A2,I2,A1)) MAIN5320
95 FORMAT (F8.1,F9.4,F9.3,I4,5X,10(F9.1)) MAIN5321

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96	FORMAT(5H1CASE15.5X17A4.9H DATE 2A6.7H TIME 2A6//	MAINS322
	1 8H TIME = F8.5.9H SECONDS //	MAINS323
	2A7. ' CRITICAL HEAT FLUX SUMMARY'//	MAINS324
	3 ' DISTANCE FLUX MONNR ROD CHANNEL'//	MAINS325
97	FORMAT(F8.1.2F8.3.2I8)	MAINS326
99	FORMAT('1CHANNEL EXIT SUMMARY RESULTS'//	MAINS327
	1 5H CASE15.5X17A4. 9H DATE 2A6.7H TIME 2A6//	MAINS328
	2 MASS BALANCE - - '17X,	MAINS329
	410X ENERGY BALANCE - - '17X,	MAINS330
	3 MASS FLOW IN ' E12.5.' LB/SEC'	MAINS331
	410X FLOW ENERGY IN 'E12.5.' BTU/SEC'//	MAINS332
	3 MASS FLOW OUT ' E12.5.' LB/SEC'	MAINS333
	410X ENERGY ADDED 'E12.5.' BTU/SEC'//	MAINS334
	3 MASS FLOW ERROR ' E12.5.' LB/SEC'	MAINS335
	410X FLOW ENERGY OUT 'E12.5.' BTU/SEC'//	MAINS336
	449X ENERGY ERROR 'E12.5.' BTU/SEC'//	MAINS337
	7 CHANNEL ENTHALPY TEMPERATURE DENSITY EQUIL VOID FLOW	MAINS338
	8 MASS FLUX'//	MAINS339
	9 (NO.) (BTU/LB) (DEG-F) (LB/FT3) QUALITY FRACTION (LB/SEC)	MAINS340
	1 (MLB/FR-FT2)'	MAINS341
100	FORMAT(I6.2F10.2.F10.2.2F9.3.F10.4.F12.4)	MAINS342
101	FORMAT(' BUNDLE AVERAGED RESULTS'//)	MAINS343
102	FORMAT(///* - - - ABNORMAL EXIT THROUGH MAXIMUM TIME - - - *//)	MAINS344
C		MAINS365
C	THE UNIVAC 1108 SETS THE CORE TO ZERO AT THE START OF EACH JOB	MAINS370
C	THE INITIALIZATION BELOW IS TO INITIALIZED FOR OTHER MACHINES	MAINS380
C	UNITS I2.I3. AND I8 ARE THE INPUT. OUTPUT, AND SAVE TAPE UNITS	MAINS390
	MC=30	MAINS400
	MG=30	MAINS410
	MX=31	MAINS420
	MN=10	MAINS430
	MR=35	MAINS440
	I2=5	MAINS450
	I3=6	MAINS460
	PI = 355./113.	MAINS470
	I8=8	MAINS475
	GC = 32.2	MAINS480
	NAXL = 0	MAINS490
	NGXL = 0	MAINS500
	NGPID = 0	MAINS510
	NAX = 0	MAINS520
	IEPDR = 0	MAINS530
	NGAPS = 0	MAINS540
	NAFACT = 0	MAINS550
	NSCRC = 0	MAINS560
	NBRC = 0	MAINS570
	J5 = 0	MAINS580
	J6 = 0	MAINS590
	NGPIDT = 0	MAINS600
	JUMP = 0	MAINS602
	NJUMP = 0	MAINS604
	NROD = 0	MAINS610
	NRAM = 1	MAINS620
	NDESE = 0	MAINS630
	NFEELT = 0	MAINS640
	NOUT = 0	MAINS650
	NPCAN = 0	MAINS660
	NPNOTE = 0	MAINS670
	NAPAMP = 1	MAINS675

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IG = 0
ISAVE = 0
IM = 0
GRID = .FALSE.
DO 900 I=1,MC
HINLET(I) = 0.
FINLET(I) = 0.
900 OPPIM(I) = 0.
DO 905 K=1,MG
905 FDIV(K) = .FALSE.
DO 930 J=1,MX
DO 910 I=1,MC
P(I,J) = 0.
H(I,J) = 0.
F(I,J) = 0.
RHO(I,J) = 0.
HOLD(I,J) = 0.
FOLD(I,J) = 0.
910 RHOOLD(I,J) = 0.
DO 915 K=1,MG
W(K,J) = 0.
WOLD(K,J) = 0.
915 SP(K,J) = 0.
DO 920 N=1,MR
FLUX(N,J) = 0.
CCHANL(N,J) = 0
DO 918 L=1,MN
918 TROP(L,N,J) = 0.
920 CONTINUE
930 CONTINUE
READ (12,52) MAXT
IF(MAXT.LT.1) MAXT = 1000

C
C READ CASE CONTROL CARD
990 READ(12,2) KASE,J1,TEXT
IFERROR = 0
ISAVE = 0
DO 991 I = 1,11
PRINT(I) = .FALSE.
IF(J1.EQ.1) PRINT(I) = .TRUE.
991 CONTINUE
C CHECK FOR CONTINUATION OF CALCULATIONS
IF(KASE.LT.1) STOP
CALL DOY(DATE)
CALL TOD(TIME)
WRITE(13, 3) KASE,TEXT,DATE,TIME

C
C READ GROUP CONTROL CARD
995 READ(12,1) NGROUP,N1,N2,N3,N4,N5,N6
IF(NGROUP.LT.1) GO TO 250
IF(NGROUP.GT.12) GO TO 240
IF(NGROUP.LT. 0) GO TO 240
GO TO (110,120,130,140,150,160,170,180,190,200,210,220),NGROUP

C
C INPUT FOR CARD GROUP 1, PROPERTY TABLE
110 READ (12,4) (PP(I),TT(I),VVF(I),VVG(I),HHF(I),HHG(I),UUF(I),KKF(I),
1,SSIPMA(I),I=1,N1)
NPROP = N1
IF(J1.LE.1) PRINT(1)=.TRUE.

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MAIN5680
MAIN5685
MAIN5690
MAIN5700
MAIN5710
MAIN5720
MAIN5730
MAIN5740
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MAIN5760
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MAIN5980
MAIN5990
MAIN6000
MAIN6010
MAIN6015
MAIN6020
MAIN6030
MAIN6040
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MAIN6060
MAIN6070
MAIN6080
MAIN6090
MAIN6100
MAIN6110
MAIN6120
MAIN6130
MAIN6150
MAIN6160
MAIN6170
MAIN6180
MAIN6190
MAIN6200
MAIN6210
MAIN6220
MAIN6230
MAIN6240

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GO TO 995	MAIN6250
C	MAIN6260
C INPUT FOR CARD GROUP 2. FRICTION FACTOR AND TWO-PHASE FLOW CORRELATION	MAIN6270
120 READ (I2,5) (AA(I),BH(I),CC(I),I=1,4)	MAIN6280
J2 = N1	MAIN6290
J3 = N2	MAIN6300
J4 = N3	MAIN6310
NVISCW = N4	MAIN6320
IF(J3.GT.4) READ(I2,4) NV,AV	MAIN6330
IF(J4.GT.4) READ(I2,4) NF,AF	MAIN6340
IF(J1.LE.1) PRINT(2) = .TRUE.	MAIN6350
GO TO 995	MAIN6360
C	MAIN6370
C INPUT FOR CARD GROUP 3. AXIAL HEAT FLUX TABLE	MAIN6380
130 READ(I2,5) (Y(I),AXIAL(I),I=1,N1)	MAIN6390
NAX = N1	MAIN6400
IF(J1.LE.1) PRINT(3) = .TRUE.	MAIN6410
GO TO 995	MAIN6420
C	MAIN6430
C INPUT FOR CARD GROUP 4. CHANNEL LAYOUT AND DIMENSIONS	MAIN6440
140 DO 141 J=1,N1	MAIN6450
READ(I2,7) N,I,AC(I),PW(I),PH(I),(LC(I,L),GAPS(I,L),DIST(I,L),	MAIN6460
1 L=1,4)	MAIN6470
NTYPE(I) = N	MAIN6480
IF(N.LE.1) NTYPE(I) = 1	MAIN6490
141 CONTINUE	MAIN6500
PHTOT = 0.	MAIN6510
ATOTAL = 0.	MAIN6520
K=0	MAIN6530
NCHANL = N2	MAIN6540
DO 147 I=1,NCHANL	MAIN6550
DO 146 L=1,4	MAIN6560
IF(LC(I,L))144,146,143	MAIN6570
143 J=LC(I,L)	MAIN6580
IF(J.LE.I) GO TO 146	MAIN6590
K=K+1	MAIN6600
FACTOR(K)=1.	MAIN6610
GO TO 145	MAIN6620
144 J=-LC(I,L)	MAIN6630
IF(J.LE.I) GO TO 146	MAIN6640
K=K+1	MAIN6650
FACTOR(K) = .5	MAIN6660
145 JK(K) = J	MAIN6670
IK(K) = I	MAIN6680
GAPN(K) = GAPS(I,L)/12.	MAIN6690
GAP(K) = GAPN(K)	MAIN6700
LENGTH(K) = DIST(I,L)/12.	MAIN6710
146 CONTINUE	MAIN6720
PERIM(I) = PW(I)/12.	MAIN6730
HPERIM(I) = PH(I)/12.	MAIN6740
AN(I) = AC(I)/144.	MAIN6750
A(I) = AN(I)	MAIN6760
DC(I) = 4.*AC(I)/PW(I)	MAIN6770
DHYD(I) = DC(I)/12.	MAIN6780
DHYDN(I) = DHYD(I)	MAIN6790
PHTOT = PHTOT + HPERIM(I)	MAIN6800
147 ATOTAL = ATOTAL + AN(I)	MAIN6810
N=K	MAIN6820
IF(J1.LE.1) PRINT(4) = .TRUE.	MAIN6830

GO TO 995	MAIN6840
C	MAIN6850
C INPUT FOR CARD GROUP 5, CHANNEL AREA VARIATION TABLE	MAIN6860
150 DO 151 I=1,NCHANL	MAIN6870
151 IDAREA(I) = 0	MAIN6880
MAXL = N2	MAIN6890
NARAMP = N3	MAIN6894
IF(NARAMP.LE.0) NARAMP = 1	MAIN6895
IF(N2.LT.1) GO TO 995	MAIN6900
READ(I2,5) (AXL(I),I=1,N2)	MAIN6910
NAFACT=N1	MAIN6920
DO 152 J=1,N1	MAIN6930
READ(I2,8) I.(AFACT(J,L),L=1,N2)	MAIN6940
IDAREA(I) = J	MAIN6950
152 NCH(J) = I	MAIN6960
IF(J1.LE.1) PRINT(5) = .TRUE.	MAIN6970
GO TO 995	MAIN6980
C	MAIN6990
C INPUT FOR CARD GROUP 6, GAP SIZE VARIATIONS TABLE	MAIN7000
160 DO 161 K=1,NK	MAIN7010
161 IDGAP(K) = 0	MAIN7020
NGXL = N2	MAIN7030
IF(N2.LT.1) GO TO 995	MAIN7040
READ(I2,5) (GAPXL(L),L=1,NGXL)	MAIN7050
NGAPS = N1	MAIN7060
DO 162 LL=1,NGAPS	MAIN7070
READ(I2,1) K	MAIN7080
IDGAP(K) = LL	MAIN7090
NGAP(LL) = K	MAIN7100
READ(I2, 5) (GFACT(LL,L),L=1,NGXL)	MAIN7110
162 CONTINUE	MAIN7120
IF(J1.LE.1) PRINT(6) = .TRUE.	MAIN7130
GO TO 995	MAIN7140
C	MAIN7150
C INPUT FOR CARD GROUP 7, SPACER DESIGN INFORMATION	MAIN7160
170 J6 = N1	MAIN7170
NRAMP = N4	MAIN7180
IF(NRAMP.LT.1) NRAMP = 1	MAIN7190
GRID = .FALSE.	MAIN7200
NGRID = 0	MAIN7210
IF(J6.EQ.0) GO TO 995	MAIN7220
IF(J6.EQ.1) GO TO 171	MAIN7230
IF(J6.EQ.2) GO TO 176	MAIN7240
GO TO 995	MAIN7250
171 READ(I2,42) PITCH,DIA,THICK	MAIN7260
PITCH = PITCH/12.	MAIN7270
DIA = DIA/12.	MAIN7280
THICK = THICK/12.	MAIN7290
NRAMP = N5	MAIN7300
DO 172 M=1,NK	MAIN7310
READ(I2,64) K,DUM,CROSS	MAIN7320
DUM(K) = DUM	MAIN7330
DO 172 L=1,6	MAIN7340
172 XCROSS(K,L) = CROSS(L)	MAIN7350
READ(I2,68) (NWRAP(I),I=1,NCHANL)	MAIN7360
DO 173 I=1,NCHANL	MAIN7370
173 NWRAPS(I) = NWRAP(I)	MAIN7380
IF(J1.LE.1) PRINT(7) = .TRUE.	MAIN7390
IF(NJUMP.EQ.3) JUMP = 3	MAIN7391

IF(NJUMP.NE.3) GO TO 995	MAIN7392
REWIND I8	MAIN7393
READ(I8) W,P,RHO,F	MAIN7394
REWIND I8	MAIN7395
GO TO 995	MAIN7400
176 NGRID = N2	MAIN7410
NGRIDT = N3	MAIN7420
READ(I2,66) (GRIDXL(I),IGRID(I),I=1,NGRID)	MAIN7430
DO 178 I=1,NGRIDT	MAIN7440
DO 177 K=1,NK	MAIN7450
177 FXFLOW(K,I) = 0.	MAIN7460
DO 178 II=1,NCHANL	MAIN7470
178 READ(I2,67) J,CD(J,I),K,FXFLOW(K,I)	MAIN7480
IF(JI.LE.1) PRINT(7) = .TRUE.	MAIN7490
GO TO 995	MAIN7500
C	MAIN7510
C INPUT FOR CARD GROUP 8, ROD LAYOUT, DIMENSIONS, AND POWER FACTORS	MAIN7520
180 NROD = N2	MAIN7530
DO 181 J=1,N1	MAIN7540
READ I1, N,I,DR(I),RADIAL(I),(LR(I,L),PHI(I,L),L=1,6)	MAIN7550
IDFUEL(I) = N	MAIN7560
IF(N.LT.1) IDFUEL(I) = 1	MAIN7570
181 CONTINUE	MAIN7580
DO 182 I=1,MC	MAIN7590
DO 182 J=1,MR	MAIN7600
182 PWRF(I,J) = 0.	MAIN7610
DO 185 I=1,NROD	MAIN7620
DO 184 L=1,6	MAIN7630
IF(LP(I,L))184,184,183	MAIN7640
183 K = LR(I,L)	MAIN7650
PWRF(K,I)=PHI(I,L)	MAIN7660
184 CONTINUE	MAIN7670
185 D(I) = DR(I)/12.	MAIN7680
IF(JI.LE.1) PRINT(8) = .TRUE.	MAIN7690
NODESF = N3	MAIN7730
NFUELT = N4	MAIN7740
NCHF = N5	MAIN7745
IF(NODESF.EQ.0) GO TO 995	MAIN7750
READ 79. (KFUEL(I), CFUEL(I), RFUEL(I), DFUEL(I),	MAIN7760
1 KCLAD(I), CCLAD(I), RCLAD(I), TCLAD(I), HGAP(I),I=1,NFUELT)	MAIN7770
DO 187 I = 1,NFUELT	MAIN7771
KFUEL(I) = KFUEL(I)/3600.	MAIN7772
KCLAD(I) = KCLAD(I)/3600.	MAIN7773
DFUEL(I) = DFUEL(I)/12.	MAIN7774
TCLAD(I) = TCLAD(I)/12.	MAIN7775
HGAP(I) = HGAP(I)/3600.	MAIN7776
187 CONTINUE	MAIN7777
GO TO 995	MAIN7780
C	MAIN7790
C INPUT FOR CARD GROUP 9, CALCULATION VARIABLES	MAIN7800
190 READ 14. KIJ,FTM,Z,THETA,NDX,NDT,TTIME,NTRIES,FERROR,SL	MAIN7810
IF(SL.LT.1.E-5) SL = .5	MAIN7820
ELEV = COS(THETA*PI/180.)	MAIN7830
IF(NTRIES,LT.1) NTRIES=20	MAIN7840
IF(FERROR.LE.0) FERROR = 1.E-3	MAIN7850
NDXPI = NDX + 1	MAIN7860
NSKIPK = N1	MAIN7870
NSKIPJ = N2	MAIN7880
KDERIG = N3	MAIN7890

IF(NSKIPT.LT.1) NSKIPT = 1	MAIN7895
IF(NSKIPX.LT.1) NSKIPX = 1	MAIN7900
ZZ = Z	MAIN7910
Z = Z/12.	MAIN7920
IF(7.LF.0.) GO TO 240	MAIN7930
IF(NDX.LT.1) GO TO 240	MAIN7940
DX = Z/FLOAT(NDX)	MAIN7950
DT = 0.	MAIN7960
IF(NDT.GT.0 .AND. TTIME.LE.0.) NDT = 0	MAIN7970
IF(NDT.GT.0) DT = TTIME/FLOAT(NDT)	MAIN7980
SAVEDT = DT	MAIN7990
DX = DX*12.	MAIN8000
IF(J1.LE.1) PRINT(9) = .TRUE.	MAIN8010
GO TO 995	MAIN8020
C	MAIN8030
C INPUT FOR CARD GROUP 10. MIXING PARAMETERS	MAIN8040
200 NSCBC = N1	MAIN8050
READ(I2,5) ABETA,BBETA	MAIN8060
NBHC =N2	MAIN8070
J5 = N3	MAIN8080
IF(N2.GE.2) READ(I2,5) (XQUAL(I),BX(I),I=1,N2)	MAIN8090
IF(J5.EQ.0) GK = 0.	MAIN8100
IF(J5.EQ.1) READ(I2,5) GK	MAIN8110
IF(J1.LE.1) PRINT(10) = .TRUE.	MAIN8120
GO TO 995	MAIN8130
C	MAIN8140
C INPUT FOR CARD GROUP 11. OPERATING CONDITIONS AND TRANSIENT FORCING	FMAIN8150
210 READ(I2,9) PEXIT,HIN,GIN,AFLUX	MAIN8160
PREF = PEXIT	MAIN8170
CALL PROP(1,1)	MAIN8180
IF(IERROR.GT.1) GO TO 240	MAIN8190
IM = N1	MAIN8200
C FOR N1=0. HIN IS THE INLET H. FOR N1=1, HIN IS THE INLET T.	MAIN8210
C FOR N1=2, READ IN CHANNEL H. FOR N1=3, READ IN CHANNEL T.	MAIN8220
IF(N1.GE.2) GO TO 214	MAIN8230
IF(N1.EQ.1) GO TO 211	MAIN8240
TIN = TF	MAIN8250
IF(HIN.LT.HF) CALL CURVE(TIN,HIN,TT,HMF,NPROP,IERROR,1)	MAIN8260
IF(IERROR.GT.1) GO TO 240	MAIN8270
GO TO 212	MAIN8280
211 TIN = HIN	MAIN8290
CALL CURVE(HIN,TIN,HMF,TT,NPROP,IERROR,1)	MAIN8300
IF(IERROR.GT.1) GO TO 240	MAIN8310
212 DO 213 I=1,NCHANL	MAIN8320
213 HINLET(I) = HIN	MAIN8330
GO TO 216	MAIN8340
214 READ(I2,10) (HINLET(I),I=1,NCHANL)	MAIN8350
IF(N1.LE.2) GO TO 216	MAIN8360
DO 215 I=1,NCHANL	MAIN8370
CALL CURVE (HINLET(I),HINLET(I),HMF,TT,NPROP,IERROR,1)	MAIN8380
IF(IERROR.GT.1) GO TO 240	MAIN8390
215 CONTINUE	MAIN8400
216 DO 2160 I=1,NCHANL	MAIN8410
TINLET(I) = TF	MAIN8412
IF(HINLET(I).LT.HF)	MAIN8414
1 CALL CURVE(TINLET(I),HINLET(I),TT,HMF,NPROP,IERROR,1)	MAIN8416
IF(IERROR.GT.1) GO TO 240	MAIN8417
2160 CONTINUE	MAIN8418
IG = N2	MAIN8419

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C FOR N2=0, GIN IS THE INLET 6 FOR EACH CHANNEL. FOR N2=1, GIN IS THE MAIN8420
C AVERAGE 6 BUT THE CHANNEL FLOWS ARE SPLIT TO GIVE EQUAL DP/DX. FOR MAIN8430
C INDIVIDUAL CHANNEL TOTAL FLOW FRACTION IS READ AS INPUT
      FLO = GIN/.0036*ATOTAL
      DO 217 I=1,NCHANL
      217 F1NET(I) = GIN*AN(I)/.0036
      F1ERROR,G1) GO TO 240
      F1ERROR,G1) GO TO 219
      F1ERROR,G1) GO TO 219
      READ(12,10) (FSPLIT(I),I=1,NCHANL)
      DO 218 I=1,NCHANL
      218 F1NET(I) = GIN*AN(I)*FSPLIT(I)/.0036
      NP = N3
      IF(NP,G1,1) READ(12,10) (FP(I),I=1,NP)
      NH = N4
      IF(NH,G1,1) READ(12,10) (FH(I),I=1,NH)
      NG = N5
      IF(NG,G1,1) READ(12,10) (FG(I),I=1,NG)
      NQ = N6
      IF(NQ,G1,1) READ(12,10) (FQ(I),I=1,NQ)
      IF(J1,LE,2) PRINT(11) = .TRUE.
      GO TO 995
C INPUT FOR CARD GROUP 12, OUTPUT OPTIONS FOR CALCULATIONS
      220 MOUT = N1
      NPCMAN = N2
      IF(N2,LT,1) GO TO 221
      READ(12,17) (PRINC(I),I=1,N2)
      221 NPROD = N3
      NPNODE = N4
      IF(N3,LT,1) GO TO 222
      READ 17, (PRINTR(I),I=1,N3)
      222 IF(N4,LT,1) GO TO 225
      READ 17, (PRIN(I),I=1,N4)
      225 GO TO 995
C INPUT DATA ERROR MESSAGE
      240 PRINT 54
      STOP
C END OF INPUT
      SET UP VARIABLES FOR OUTPUT PRINTOUT
      250 DO 251 I=1,NCHANL
      4(I) = AN(I)
      251 DRYD(I) = DRYD(I)
      DO 252 K=1,NK
      252 GAP(K) = GAP(K)
      IF(NPCMAN,G1,0) GO TO 257
      NPCMAN = NCHANL
      DO 256 I=1,NCHANL
      256 PRINT(I) = I
      257 IF(NPROD,G1,0) GO TO 259
      NPROD = NPROD
      DO 258 N=1,NPROD
      258 PRINT(N) = N
      259 IF(NNODE,G1,0) GO TO 261
      NM = NODESF*1

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MAIN9010  
 MAIN9000  
 MAIN8990  
 MAIN8980  
 MAIN8970  
 MAIN8950  
 MAIN8940  
 MAIN8930  
 MAIN8920  
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 MAIN8900  
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 MAIN8710  
 MAIN8700  
 MAIN8690  
 MAIN8680  
 MAIN8670  
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 MAIN8530  
 MAIN8520  
 MAIN8510  
 MAIN8500  
 MAIN8490  
 MAIN8480  
 MAIN8470  
 MAIN8460  
 MAIN8450  
 MAIN8440



NPNODE = NN	MAIN9020
DO 260 I=1,NN	MAIN9030
260 PRINTN(I) = I	MAIN9040
C	MAIN9050
C OUTPUT OF INPUT DATA	MAIN9060
C	MAIN9070
261 IF(.NOT.PRINT(1)) GO TO 265	MAIN9080
WRITE(I3,13) (PP(I),TT(I),VVF(I),VVG(I),HHF(I),HMG(I),UJF(I),	MAIN9090
IKKF(I),SSIGMA(I),I=1,NPROP)	MAIN9100
265 IF(.NOT.PRINT(2)) GO TO 270	MAIN9110
WRITE(I3,28)	MAIN9120
DO 266 J=1,4	MAIN9130
IF(AA(J).GT.0. .OR. CC(J).GT.0.) WRITE(I3,29) J,AA(J),BB(J),CC(J)	MAIN9140
266 CONTINUE	MAIN9150
IF(NVISCW.EQ.0) WRITE(I3,61)	MAIN9160
IF(NVISCW.EQ.1) WRITE(I3,62)	MAIN9170
WRITE(I3,44)	MAIN9180
IF(J2.EQ.0) WRITE(I3,45)	MAIN9190
IF(J2.EQ.1) WRITE(I3,46)	MAIN9200
IF(J3.EQ.0) WRITE(I3,47)	MAIN9210
IF(J3.EQ.1) WRITE(I3,48)	MAIN9220
IF(J3.EQ.5) WRITE(I3,49) AV(I)	MAIN9230
IF(J3.EQ.6) WRITE(I3,57) NV,(AV(I),I=1,NV)	MAIN9240
IF(J4.EQ.0) WRITE(I3,58)	MAIN9250
IF(J4.EQ.1) WRITE(I3,59)	MAIN9260
IF(J4.EQ.5) WRITE(I3,60) NF,(AF(I),I=1,NF)	MAIN9270
270 IF(.NOT.PRINT(3)) GO TO 275	MAIN9280
WRITE(I3,6) (Y(I),AXIAL(I),I=1,NAX)	MAIN9290
275 IF(.NOT.PRINT(4)) GO TO 280	MAIN9300
WRITE(I3,12) (I,NTYPE(I),AC(I),PW(I),PH(I),DC(I),(LC(I),L),	MAIN9310
1 GAPS(I,L),DIST(I,L),L=1,4),I=1,NCHANL)	MAIN9320
280 IF(NAXL .LT.1) GO TO 285	MAIN9330
IF(.NOT.PRINT(5)) GO TO 285	MAIN9340
N=1	MAIN9350
NN=10	MAIN9360
DO 284 LL=1,4	MAIN9370
IF(NN.GT.NAFACT) NN = NAFACT	MAIN9380
WRITE(I3,19) ((H1,NCH(J),H3),J=N,NN)	MAIN9390
DO 283 I=1,NAXL	MAIN9400
283 WRITE(I3,34) AXL(I), (AFACT(J,I),J=N,NN)	MAIN9410
N=N+10	MAIN9420
NN=NN+10	MAIN9430
IF(N.GF.NAFACT) GO TO 285	MAIN9440
244 CONTINUE	MAIN9450
285 IF(NGXL .LT.1) GO TO 290	MAIN9460
IF(.NOT.PRINT(6)) GO TO 290	MAIN9470
N = 1	MAIN9480
NN= 10	MAIN9490
DO 289 LL = 1,6	MAIN9500
IF(NN.GT.NGAPS) NN=NGAPS	MAIN9510
DO 286 M=N,NN	MAIN9520
K = NGAP(M)	MAIN9530
IM(M) = IK(K)	MAIN9540
286 JM(M) = JK(K)	MAIN9550
WRITE(I3,20) ((H1,IM(M),H2,JM(M),H3),M=N,NN)	MAIN9560
DO 287 L=1,NGXL	MAIN9570
287 WRITE(I3,38) GAPXL(L),(GFACT(M,L),M=N,NN)	MAIN9580
N=N+10	MAIN9590
NN=NN+10	MAIN9600

IF(N.GE.NGAPS) GO TO 290	MAIN9610
289 CONTINUE	MAIN9620
290 IF(.NOT.PRINT(7)) GO TO 300	MAIN9630
IF(J6.EQ.0) GO TO 300	MAIN9640
IF(J6.GT.1) GO TO 296	MAIN9650
PITCH = PITCH*12.	MAIN9660
DIA = DIA*12.	MAIN9670
THICK = THICK*12.	MAIN9680
PRINT 69, PITCH, THICK, DIA	MAIN9690
PITCH = PITCH/12.	MAIN9700
DIA = DIA/12.	MAIN9710
THICK = THICK/12.	MAIN9720
PRINT 70, (K,H1,IK(K),H2,JK(K),H3,DUR(K),(XCPOSS(K,L),L=1,6),	MAIN9730
1 K=1,NK)	MAIN9740
PRINT 74, (NWRAP(I),I=1,NCHANL)	MAIN9750
GO TO 300	MAIN9760
296 PRINT 71, (IGRID(I),I=1,NGRID)	MAIN9770
PRINT 72, (GRIDXL(I),I=1,NGRID)	MAIN9780
DO 297 L=1,NGRIDT	MAIN9790
297 PRINT 73, L,(I,CD(I,L),I=1,NCHANL)	MAIN9800
DO 299 I=1,NGRIDT	MAIN9810
II = 0	MAIN9820
DO 298 K=1,NK	MAIN9830
IF(ABS(FXFLOW(K,I)).GT.0) II=1	MAIN9840
298 CONTINUE	MAIN9850
IF(II.EQ.0) GO TO 299	MAIN9860
PRINT 76, I,(KK,H1,IK(KK),H2,JK(KK),H3,FXFLOW(KK,I),KK=1,NK)	MAIN9870
299 CONTINUE	MAIN9880
300 IF(.NOT.PRINT(8)) GO TO 305	MAIN9890
PRINT 15, (I,IDFUEL(I),DR(I),RADIAL(I),(PHI(I,L),LR(I,L),	MAIN9900
1 L=1,6),I=1,NROD)	MAIN9910
IF(NODESF.LT.1) GO TO 305	MAIN9920
DO 301 I = 1,NFUELT	MAIN9921
KFUEL(I) = KFUEL(I)*3600.	MAIN9922
KCLAD(I) = KCLAD(I)*3600.	MAIN9923
DFUEL(I) = DFUEL(I)*12.	MAIN9924
TCLAD(I) = TCLAD(I)*12.	MAIN9925
HGAP(I) = HGAP(I)*3600.	MAIN9926
301 CONTINUE	MAIN9927
PRINT 77, NODESF	MAIN9930
PRINT 78, (J,KFUEL(J),CFUEL(J),RFUEL(J),DFUEL(J),KCLAD(J),CCLAD(J),	MAIN9940
1,PCLAD(J),TCLAD(J),HGAP(J),J=1,NFUELT)	MAIN9950
DO 302 I = 1,NFUELT	MAIN9960
KFUEL(I) = KFUEL(I)/3600.	MAIN9970
KCLAD(I) = KCLAD(I)/3600.	MAIN9980
DFUEL(I) = DFUEL(I)/12.	MAIN9990
TCLAD(I) = TCLAD(I)/12.	MAIN0000
HGAP(I) = HGAP(I)/3600.	MAIN0010
302 CONTINUE	MAIN0020
305 IF(.NOT.PRINT(9)) GO TO 310	MAIN0030
PRINT 18, KIJ,FTM,SL,ZZ,THETA,NDX,DXX,NDT,TTIME,DT,NTRIES,FERROR	MAIN0040
310 IF(.NOT.PRINT(10))GO TO 315	MAIN0050
WRITE(I3,35)	MAIN0060
IF(NSCHC.LT.1) WRITE(I3, 32) ABETA	MAIN0070
IF(NSCHC.EQ.1) WRITE(I3, 33) ABETA, BBETA	MAIN0080
IF(NSCHC.EQ.2) WRITE(I3, 34) ABETA, BBETA	MAIN0090
IF(NSCHC.EQ.3) WRITE(I3,39) ABETA, BBETA	MAIN0100
IF(NSCHC-1) 311,311,312	MAIN0110
311 WRITE(I3,36)	MAIN0120

	GO TO 314	MAIN0130
312	WRITE (I3,37) (XQUAL(I),BX(I),I=1,NBNC)	MAIN0140
314	IF(JS.FQ.1) PRINT 65, GK	MAIN0150
315	IF(.NOT.PRINT(11)) GO TO 318	MAIN0160
	WRITE(I3,21) PEXIT,HIN,GIN,TIN,AFLUX	MAIN0170
	IF(IH.FQ.0) WRITE(I3,87)	MAIN0180
	IF(IH.EQ.1) WRITE(I3,88)	MAIN0190
	IF(IH.EQ.2) WRITE(I3,89)	MAIN0200
	IF(IH.EQ.3) WRITE(I3,90)	MAIN0210
	IF(IG.FQ.0) WRITE(I3,91)	MAIN0220
	IF(IG.EQ.1) WRITE(I3,92)	MAIN0230
	IF(IG.EQ.2) WRITE(I3,93)	MAIN0240
	IF(NP.GT.1) PRINT 83, (YP(I),FP(I),I=1,NP)	MAIN0250
	IF(NH.GT.1) PRINT 84, (YH(I),FH(I),I=1,NH)	MAIN0260
	IF(NG.GT.1) PRINT 85, (YG(I),FG(I),I=1,NG)	MAIN0270
	IF(NQ.GT.1) PRINT 86, (YQ(I),FQ(I),I=1,NQ)	MAIN0280
318	IF(KDERUG) 400,400,319	MAIN0290
319	WRITE(I3,50) ((LC(I,L),I=1,NCHANL),L=1,4)	MAIN0300
	WRITE(I3,50) (IK(K),JK(K),K=1,NK)	MAIN0310
	WRITE(I3,51) (FACTOR(K),K=1,NK)	MAIN0320
	WRITE(I3,50) ((LR(NR,L),NR=1,NROD),L=1,6)	MAIN0330
	WRITE(I3,51) ((PWRF(I,NR),NR=1,NROD),I=1,NCHANL)	MAIN0340
	WRITE(I3,51) (D(NR),NR=1,NROD),(RADIAL(NR),NR=1,NROD)	MAIN0350
C		MAIN0360
C	START SURCHANNEL FLOW AND ENTHALPY CALCULATIONS.	MAIN0370
400	KT = MSKIPT	MAIN1280
	DT = SAVEDT	MAIN1290
	DO 401 J=1,NDXP1	MAIN1300
401	X(J) = DX*FLOAT(J-1)	MAIN1302
	NDTP1 = NDT+1	MAIN1304
	DO 500 NT=1,NDTP1	MAIN1306
	IERROR = 0	MAIN1310
	DT = SAVEDT	MAIN1314
	IF(NT.EQ.1) DT = 1.E+10	MAIN1315
	ETIME = DT*FLOAT(NT-1)	MAIN1320
C	ESTABLISH CHANNEL BOUNDARY CONDITIONS AND FORCING FUNCTION VALUES.	MAIN1330
	DUMY = 1.	MAIN1340
	IF(NP.GT.1)	MAIN1350
	1CALL CURVE (DUMY,ETIME,FP,YP,NP,IERROR,1)	MAIN1360
	IF(IERROR.GT.1) GO TO 505	MAIN1370
	PREF = DUMY*PEXIT	MAIN1380
	CALL PROP(1,1)	MAIN1390
	IF(IERROR.GT.1) GO TO 505	MAIN1400
	DUMY = 1.	MAIN1410
	IF(NH.GT.1)	MAIN1420
	1CALL CURVE (DUMY,ETIME,FH,YH,NH,IERROR,1)	MAIN1430
	IF(IERROR.GT.1) GO TO 505	MAIN1440
	DO 402 I=1,NCHANL	MAIN1450
	HOLD(I,1) = H(I,1)	MAIN1460
	H(I,1) = HINLET(I)*DUMY	MAIN1470
	IF(IH.EQ.1 .OR. IH.EQ.3)	MAIN1472
	1 CALL CURVE (H(I,1),TINLET(I)*DUMY,HMF,TT,NPROP,IERROR,1)	MAIN1476
402	CONTINUE	MAIN1478
	DUMY = 1.	MAIN1480
	IF(NG.GT.1)	MAIN1490
	1 CALL CURVE (DUMY,ETIME,FG,YG,NG,IERROR,1)	MAIN1500
	IF(IERROR.GT.1) GO TO 505	MAIN1510
	DO 403 I=1,NCHANL	MAIN1520
	FOLD(I,1) = F(I,1)	MAIN1530

403 F(I,1) = FINLET(I)*DUMY	MAIN1540
DUMY = 1.	MAIN1550
IF(NO.GT.1)	MAIN1560
1CALL CURVE (DUMY,ETIME,FQ,Y3,NO,IERROR,1)	MAIN1570
IF(IERROR.GT.1) GO TO 505	MAIN1580
POWER = DUMY	MAIN1590
C	MAIN1600
C BEGIN ITERATION TO OBTAIN SOLUTION.	MAIN1605
DO 430 NN=1,NTRIES	MAIN1610
DO 410 I=1,NCHANL	MAIN1620
410 NWRAP(I) = NWRAPS(I)	MAIN1630
ITERAT = NN	MAIN1640
CALL SCHEMF(JUMP)	MAIN1650
IF(IERROR.GT.1) GO TO 440	MAIN1660
CALL FLAP(MTIME)	MAIN1662
IF(MTIME.LT.MAXT) GO TO 429	MAIN1664
PRINT 102	MAIN1666
GO TO 440	MAIN1668
429 IF(JUMP.LT.1 .OR. JUMP.GT.3) GO TO 505	MAIN1670
GO TO (430,440,440),JUMP	MAIN1680
430 CONTINUE	MAIN1690
PPRINT 22, NTRIES	MAIN1700
IERROR = 1	MAIN1710
C SET CONDITIONS FOR NEXT TIME STEP	MAIN1720
440 IF(JUMP.EQ.3) GO TO 441	MAIN1730
IF(NJUMP.GT.0) JUMP = 3	MAIN1731
IF(NJUMP.NE.2) GO TO 441	MAIN1732
REWIND I8	MAIN1733
WRITE(I8) W,P,RHO,F	MAIN1734
END FILE I8	MAIN1735
REWIND I8	MAIN1736
441 DO 445 J=1,NDXP1	MAIN1737
DO 443 K=1,NK	MAIN1740
WOLD(K,J) = W(K,J)	MAIN1750
443 CONTINUE	MAIN1760
DO 444 I=1,NCHANL	MAIN1770
FOLD(I,J) = F(I,J)	MAIN1780
HOLD(I,J) = H(I,J)	MAIN1790
RHOOLD(I,J) = RHO(I,J)	MAIN1800
444 CONTINUE	MAIN1810
445 CONTINUE	MAIN1820
ISAVE = IERROR	MAIN1822
IERROR = 0	MAIN1824
IF(NCHF.GT.0 .AND. ISAVE.EQ.0) CALL CHF(3,NDXP1)	MAIN1826
KT = KT+1	MAIN1830
IF(KT.LT.NSKIPT) GO TO 500	MAIN1840
CALL TOD(TIME)	MAIN1850
C	MAIN1856
C PRINT RESULTS	MAIN1857
IF(ETIME.GT.0.) GO TO 457	MAIN1858
C COMPUTE MASS AND ENERGY BALANCE	MAIN1859
FLOIN = 0.	MAIN1860
FLOOUT = 0.	MAIN1861
ENGIN = 0.	MAIN1862
ENGOUT = 0.	MAIN1863
NDXP1 = NDXP+1	MAIN1864
DO 448 I=1,NCHANL	MAIN1865
FLOIN = FLOIN + F(I,1)	MAIN1866
FLOOUT = FLOOUT + F(I,NDXP1)	MAIN1867

ENGIN = ENGIN + F(I,1)*H(I,1)	MAIN1868
448 ENGOUT = ENGOUT + F(I,NDXP1)*H(I,NDXP1)	MAIN1869
FLOERP = FLOOUT - FLOIN	MAIN1870
ENGADD = AFLUX*Z*PHTOT/.0036	MAIN1871
ENGERR = ENGOUT - ENGIN - ENGADD	MAIN1872
PRINT 99, KASE,TEXT,DATE,TIME,FLOIN,ENGIN,FLOOUT,ENGADD,FLOERP,	MAIN1873
IENGOUT,ENGERR	MAIN1874
C PREPARE CHANNEL EXIT SUMMARY	MAIN1875
J = NDXP1	MAIN1876
DO 450 I=1,NCHANL	MAIN1877
OUTPUT(1) = TF	MAIN1878
IF (H(I,J).LT.HF) CALL CURVE(OUTPUT(1),H(I,J),TT,HMF,NPROP,IEPROR,1)	MAIN1879
OUTPUT(2) = (H(I,J)-HF)/HFG	MAIN1880
IF (OUTPUT(2).LT.0.) OUTPUT(2) = 0.	MAIN1881
OUTPUT(3) = (RHOF-RHO(I,J))/(RHOF-RHOG)	MAIN1882
IF (OUTPUT(3).LT.0.) OUTPUT(3) = 0.	MAIN1883
OUTPUT(4) = F(I,J)/AN(I)*.0036	MAIN1884
PRINT 100, I,H(I,J),OUTPUT(1),RHO(I,J),OUTPUT(2),OUTPUT(3),	MAIN1885
I F(I,J),OUTPUT(4)	MAIN1886
450 CONTINUE	MAIN1887
IF (IEPROR.GT.1) GO TO 505	MAIN1888
C COMPUTE BUNDLE AVERAGED RESULTS	MAIN1889
452 PRINT 25, KASE,TEXT,DATE,TIME	MAIN1890
PRINT 101	MAIN1891
PRINT R2	MAIN1892
DO 456 J=1,NDXP1,NSKIPX	MAIN1893
SAVE1 = 0.	MAIN1894
SAVE2 = 0.	MAIN1895
SAVE3 = 0.	MAIN1896
SAVE4 = 0.	MAIN1897
DO 454 I=1,NCHANL	MAIN1898
SAVE1 = SAVE1 + P(I,J)*AN(I)	MAIN1899
SAVE2 = SAVE2 + H(I,J)*F(I,J)	MAIN1900
SAVE3 = SAVE3 + F(I,J)	MAIN1901
454 SAVE4 = SAVE4 + RHO(I,J)*AN(I)	MAIN1902
OUTPUT(1) = X(J)*12.	MAIN1903
OUTPUT(2) = SAVE1/ATOTAL/144.	MAIN1904
OUTPUT(3) = SAVE2/SAVE3	MAIN1905
OUTPUT(4) = TF	MAIN1906
IF (OUTPUT(3).LT.HF) CALL CURVE(OUTPUT(4),OUTPUT(3),TT,HMF,NPROP,	MAIN1907
I IERROR,1)	MAIN1908
IF (IEPROR.GT.1) GO TO 505	MAIN1909
OUTPUT(5) = SAVE4/ATOTAL	MAIN1910
OUTPUT(6) = 0.	MAIN1911
IF (OUTPUT(3).GT.HF) OUTPUT(6) = (OUTPUT(3)-HF)/HFG	MAIN1912
OUTPUT(7) = 0.	MAIN1913
IF (OUTPUT(5).LT.RHOF) OUTPUT(7) = (RHOF-OUTPUT(5))/(RHOF-RHOG)	MAIN1914
OUTPUT(8) = SAVE3	MAIN1915
OUTPUT(9) = SAVE3/ATOTAL*.0036	MAIN1916
PRINT R1, (OUTPUT(II),II=1,9)	MAIN1917
456 CONTINUE	MAIN1918
IF (IEPROR.GT.1) GO TO 505	MAIN1919
C PRINT CHANNEL AND ROD RESULTS AS DEFINED BY OUTPUT OPTIONS	MAIN1920
457 DO 460 JJ=1,NPCHAN	MAIN1921
I = PRINTC(JJ)	MAIN1922
PRINT 26, KASE, TEXT, DATE, TIME	MAIN1923
PRINT 40,ETIME,I	MAIN1924
PRINT R2	MAIN1925
DO 458 J=1,NDXP1,NSKIPX	MAIN1926

OUTPUT(1) = X(J)*12.	MAIN1927
OUTPUT(3) = H(I,J)	MAIN1930
OUTPUT(2) = P(I,J)/144.	MAIN1940
OUTPUT(4) = TF	MAIN1950
IF(H(I,J).LT.HF)CALL CURVE(OUTPUT(4),H(I,J),TT,MHF,NPROP,IERROR,1)	MAIN1960
IF(IERROR.GT.1) GO TO 505	MAIN1965
OUTPUT(5) = RHO(I,J)	MAIN1970
OUTPUT(6) = 0.	MAIN1980
IF(H(I,J).GT.HF) OUTPUT(6) = (H(I,J)-HF)/HFG	MAIN1990
OUTPUT(7) = 0.	MAIN2000
IF(RHO(I,J).LT.RHOF) OUTPUT(7) = (RHOF-RHO(I,J))/(RHOF-RHOG)	MAIN2010
OUTPUT(8) = F(I,J)	MAIN2020
OUTPUT(9) = F(I,J)/AN(I)*.0036	MAIN2030
PRINT 81, (OUTPUT(II),II=1,9)	MAIN2040
458 CONTINUE	MAIN2050
460 CONTINUE	MAIN2060
IF(NOUT.LT.1) GO TO 499	MAIN2070
IF(NOUT.EQ.2) GO TO 470	MAIN2080
DO 465 M=1,NK,10	MAIN2090
MM = M+9	MAIN2100
IF(NK.LE.MM) MM=NK	MAIN2110
PRINT 31, KASE, TEXT, DATE, TIME, H7, (H6,H1,IK(K),H2,JK(K),	MAIN2120
1 H3,K=M,MM)	MAIN2130
DO 465 J=1,NDXP1,NSKIPX	MAIN2140
XDUMY = X(J)*12.	MAIN2150
PRINT 30, XDUMY, (W(K,J),K=M,MM)	MAIN2160
465 CONTINUE	MAIN2170
IF(NOUT.EQ.1) GO TO 499	MAIN2180
470 IF(NPROD.LT.1) GO TO 4990	MAIN2195
DO 485 NN=1,NPROD	MAIN2190
N = PRINTR(NN)	MAIN2200
NDUMY = IDFUEL(N)	MAIN2210
PRINT 94, KASE, TEXT, DATE, TIME, ETIME, N, NDUMY,	MAIN2220
1 (H8,PRINTN(I),H3,I=1,NPNODE)	MAIN2230
DO 483 J=1,NDXP1,NSKIPX	MAIN2240
XDUMY = X(J)*12.	MAIN2250
DO 480 II=1,NPNODE	MAIN2260
I = PRINTN(II)	MAIN2270
480 TDUMY(II) = TROD(I,N,J)	MAIN2280
DFLUX = FLUX(N,J)*.0036	MAIN2290
IF(CCHANL(N,J).EQ.0) CHFR(N,J) = 0.	MAIN2292
IF(NODESF.GT.1) PRINT 95, XDUMY,DFLUX,CHFR(N,J),CCHANL(N,J),	MAIN2294
1 (TDUMY(I),I=1,NPNODE)	MAIN2296
IF(NODESF.LT.1) PRINT 95, XDUMY,DFLUX,CHFR(N,J),CCHANL(N,J)	MAIN2300
483 CONTINUE	MAIN2310
485 CONTINUE	MAIN2320
488 IF(NCHF.LT.1) GO TO 499	MAIN2321
PRINT 96, KASE,TEXT,DATE,TIME,ETIME,CHFCOR(NCHF)	MAIN2322
DO 4945 J=1,NDXP1,NSKIPX	MAIN2323
XDUMY = X(J)*12.	MAIN2324
N = MCHERR(J)	MAIN2325
DFLUX = 0.	MAIN2326
IF(N.NE.0) DFLUX = FLUX(N,J)*.0036	MAIN2327
IF(N.EQ.0) MCHFR(J) = 0.	MAIN2328
PRINT 97, XDUMY,DFLUX,MCHFR(J),MCHERR(J),MCHERC(J)	MAIN2329
4945 CONTINUE	MAIN2330
499 PRINT 75, ITERAT	MAIN2331
KI = 0	MAIN2340
IF(ISAVE.GT.0) GO TO 505	MAIN2345

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          IF(IERROR.GT.0) GO TO 505
500 CONTINUE
C
C END OF PROBLEM. LOOK FOR NEW CASE
GO TO 990
505 PRINT 55, SIGNAL(IERROR)
PRINT 55, SIGNAL(ISAVE)
GO TO 990
END
*DECK SCHEME
SUBROUTINE SCHEME(JUMP)
C
C THIS SUBROUTINE SETS UP AND PERFORMS THE SOLUTION OF THE FINITE
C DIFFERENCE SCHEME AT EACH SPATIAL LOCATION X AT A SELECTED TIME T.
C
C THIS PROCEDURE CONTAINS THE COMMON AND TYPE STATEMENTS SHARED BY THE
C MAJOR SUBROUTINES OF COBRA-IIIC.
COMMON KIJ, FTM, ABETA, BBETA, AFLUX, Z, THETA, PI, NAX, FLO,
1 GC, I3, I2, NCHANL, NK, IERROR, KDEBUG, NAXL, NGAPS, NSXL,
2 NAFAC, NODES, NSCHC, NPROC, J1, J2, J3, J4, J5, J6, J7,
3 ATOTAL, DX, DT, GK, NV, NF, AV(7), AF(7), OAX, FSPLIT(30)
4 , ELEV, NDX, SL, FERROR, ITERAT, NRAMP, NVISCW, NARAMP
COMMON PP(30), TT(30), VVF(30), VVG(30), HHF(30), HHG(30),
1 UUF(30), KKF(30), SSIGMA(30), NPROP, PREF, TF, VF, VG, HF, HG,
2 UF, KF, SIGMA, HFG, VFG, RHOF, RHOG
COMMON V(30), VP(30), VISC(30), VISCW(30), HFILM(30), CON(30),
1 CP(30), FSP(30), FMULT(30), U(30), UH(30), ALPHA(30), QUAL(30),
2 RHO(30,31), VPA(30), T(30), HINLET(30), FINLET(30)
COMMON COND(47), WP(47), GAP(47), FACTOR(47), IK(47),
1 JK(47), GAPN(47), LENGTH(47), USTAR(47), W(47,31)
COMMON A(30), AN(30), DHYD(30), DHYDN(30), DFDX(30),
1 DHDX(30), DPOX(30), QPPIM(30), PERIM(30),
2 HPERIM(30), NTYPE(30)
COMMON P(30,31), H(30,31), F(30,31), X(31)
COMMON WOLD(47,31), RHOOLD(30,31), FOLD(30,31), HOLD(30,31)
COMMON AXIAL(39), Y(39), IDAPEA(30), IDGAP(47), AA(4), BB(4),
1 CC(4), AFACT(10,10), NCH(10), AXL(10), GAPXL(10), GFACT(9,10),
2 NGAP(9), RX(30), XQUAL(30)
COMMON NGRID, NGRIDT, GRIDXL(10), IGRID(10), CD(30,5),
1 FXFLOW(47,5), NGTYPE, GRID, FDIV(47)
LOGICAL FDIV, GRID
REAL KIJ, LENGTH, KF, KKF
REAL KFUEL, KCLAD
COMMON /FUFL/ KFUEL(3), KCLAD(3), RFUEL(3), RCLAD(3),
1 CFUEL(3), CCLAD(3), TCLAD(3), TFLUID,
2 FLUX(35,31), HGAP(3), TPOD(10,35,31), LR(35,6),
3 PWRP(30,35), PHI(35,6), RADIAL(35), D(35),
4 POWER, NODESF, NROD, DFUEL(3), IDFUEL(35), HSURF
DIMENSION WSAVE(47)
COMMON /BSP/ SP(47,31)
1 FORMAT('IF ERROR DETECTED IN SUBROUTINE SCHEME AT NODE I3,
1 ' X =E10.5, FEET// CALCULATION FOR THIS CASE STOPPED')
2 FORMAT(' NODE I3, X =E10.5)
3 FORMAT(' I H(I,J) F(I,J) P(I,J) H(I,J-1)
1(I,J-1) P(I,J-1)')
4 FORMAT(' I QUAL(I) ALPHA(I) RHO(I,J) VP(I)
1 V(I) FMULT(I)')
5 FORMAT(' K W(K,J-1) W(K,J) WP(K) USTAR(K)
1(K,J-1) SP(K,J)')

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MAIN2350
MAIN2360
MAIN2370
MAIN2380
MAIN2390
MAIN2400
MAIN2405
MAIN2410
MAIN2420
SCHM0010
SCHM0020
SCHM0030
SCHM0040
SCHM0050
SCHM0060
SCHM0070
SCHM0080
SCHM0090
SCHM0100
SCHM0110
SCHM0120
SCHM0130
SCHM0140
SCHM0150
SCHM0160
SCHM0170
SCHM0180
SCHM0190
SCHM0200
SCHM0210
SCHM0220
SCHM0230
SCHM0240
SCHM0250
SCHM0260
SCHM0270
SCHM0280
SCHM0290
SCHM0300
SCHM0310
SCHM0320
SCHM0330
SCHM0340
SCHM0350
SCHM0360
SCHM0370
SCHM0380
SCHM0390
SCHM0400
SCHM0401
SCHM0402
SCHM0403
SCHM0404
SCHM0405
SCHM0406
SCHM0407
SCHM0408
SCHM0409

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6	FORMAT(' I DHDX(I) DFDX(I) DPOX(I) QPRIM(I) FOSCHM0410
	1LD(I,J) RHOOLD(I,J)')
16	FORMAT(3I5.4E12.6)
52	FORMAT( 15.6E12.6)
	NCHANL = NCHANL
	FMIN = .0001
	NDXP1 = NDX+1
	IF(JUMP.EQ.3) GO TO 400
	JUMP = 2
C	
C	BEGIN STEPPING THROUGH CHANNEL
400	DO 450 J=1,NDXP1
	JPI = J+1
	JMI = J-1
	IF(J.GT.1) GO TO 405
C	SET CONDITIONS AT START OF CHANNEL
401	DO 401 I=1,NCHANL
	QPRIM(I) = 0.
	CALL FORCE(I)
	IF(IERROR.GT.1) GO TO 440
	CALL AREA(I)
	IF(IERROR.GT.1) GO TO 440
	CALL PROP(2,I)
	IF(IERROR.GT.1) GO TO 440
	CALL VOID(I)
	IF(IERROR.GT.1) GO TO 440
	GO TO 450
405	IF(JUMP.EQ.3) GO TO 420
	IF(NGRID.LT.1) GO TO 410
	GRID = .FALSE.
	DO 408 I=1,NGRID
	ZG = GRIDXL(I)*Z
	IF(ZG.GT.X(JMI) .AND. ZG.LE.X(J)) GO TO 409
408	CONTINUE
	GO TO 410
409	NGTYPE = IGRID(I)
	GRID = .TRUE.
C	CALCULATE PARAMETERS TO BE SAVED FROM PREVIOUS SPACE
410	DO 411 I=1,NCHANL
	VPA(I) = VP(I)/A(I)
411	CONTINUE
420	CALL HEAT(J)
	IF(IERROR.GT.1) GO TO 440
	CALL MIX(JMI)
	IF(IERROR.GT.1) GO TO 440
	CALL DIFFER(1,JMI)
	IF(IERROR.GT.1) GO TO 440
C	
C	CALCULATE ENTHALPY AND ESTIMATE FLOW AT X.
425	DO 425 I=1,NCHANL
	IF(ITERAT.EQ.1 .AND. JUMP.NE.3) F(I,J) = F(I,JMI)
	H(I,J) = (H(I,JMI) + DX/DT/UH(I)*HOLD(I,J) + DX*DHDX(I))/
	1 (1.+DX/DT/UH(I))
425	CONTINUE
	IF(JUMP.EQ.3) GO TO 450
	CALL FORCE(J)
	IF(IERROR.GT.1) GO TO 440
	CALL AREA(J)
	IF(IERROR.GT.1) GO TO 440



CALL PROP(2,J)	SCHM0980
IF(IERROR.GT.1) GO TO 440	SCHM0990
CALL VOID(J)	SCHM1010
IF(IERROR.GT.1) GO TO 440	SCHM1020
CALL DIFFER(3,J)	SCHM1030
IF(IERROR.GT.1) GO TO 440	SCHM1040
DO 426 K=1,NK	SCHM1050
WSAVE(K) = W(K,J)	SCHM1060
426 CONTINUE	SCHM1070
C CALCULATE THE DIVERSION CROSSFLOW AT X.	SCHM1080
CALL DIVERT(J)	SCHM1090
IF(IERROR.GT.1) GO TO 440	SCHM1100
C CALCULATE THE FLOW AT X AND CHECK FOR CONVERGENCE.	SCHM1110
CALL DIFFER(2,J)	SCHM1160
IF(IERROR.GT.1) GO TO 440	SCHM1170
DO 4270 I=1,NCHANL	SCHM1180
FSAVE = F(I,J)	SCHM1185
F(I,J) = F(I,JM1) + DX*DFDX(I) - DX/DT*(RHO(I,J)-RHOOLD(I,J))*A(I)	SCHM1190
C THE FOLLOWING STATEMENT PROVIDES DAMPING TO ASSIST IN MORE RAPID	SCHM1191
C CONVERGENCE, ESPECIALLY WHEN USING THE SUBCOOLED VOID OPTION.	SCHM1192
C USERS MAY WISH TO TRY OTHER COMBINATIONS OF CONSTANTS.	SCHM1193
F(I,J) = .2*FSAVE + .8*F(I,J)	SCHM1194
IF(ABS(F(I,J)-FSAVE)/FSAVE.GT.FERROR) JUMP = 1	SCHM1195
IF(F(I,J).LT.FMIN) F(I,J) = FMIN	SCHM1200
4270 CONTINUE	SCHM1210
C CALCULATE SP AT X-DX.	SCHM1220
CALL DIFFER(4,J)	SCHM1230
IF(IERROR.GT.1) GO TO 440	SCHM1240
C THE FACTOR DAMPING WAS ADDED AFTER PUBLICATION. A VALUE OF ZERO WAS	SCHM1241
C USED FOR THE SAMPLE PROBLEMS. A VALUE OF 0.5 HAS BEEN FOUND TO SPEED	SCHM1242
C CONVERGENCE FOR MANY PROBLEMS. USERS MAY WISH TO TRY OTHER VALUES.	SCHM1243
DAMPNG = 0.	SCHM1244
DO 430 K=1,NK	SCHM1250
II = IK(K)	SCHM1260
JJ = JK(K)	SCHM1270
SP(K,JM1) = DAMPNG*SP(K,JM1)	SCHM1280
1 + (1.-DAMPNG)*(SP(K,J)-(DPDX(II)-DPDX(JJ))*DX)	SCHM1285
430 CONTINUE	SCHM1290
DO 428 I=1,NCHANL	SCHM1300
P(I,J) = P(I,JM1) + DX*DPDX(I)	SCHM1310
428 CONTINUE	SCHM1320
IF(KDEBUG.LT.1) GO TO 450	SCHM1330
GO TO 445	SCHM1340
440 PRINT 1, J, X(J)	SCHM1342
GO TO 446	SCHM1344
445 PRINT 2, J, X(J)	SCHM1346
446 PRINT 3	SCHM1348
PRINT 52, (I,H(I,J),F(I,J),P(I,J),H(I,JM1),F(I,JM1),P(I,JM1),	SCHM1350
1 I=1,NCHANL)	SCHM1360
PRINT 4	SCHM1365
PRINT 52, (I,QUAL(I),ALPHA(I),RHO(I,J), VP(I),V(I),FMULT(I),	SCHM1370
1 I=1,NCHANL)	SCHM1380
PRINT 5	SCHM1385
PRINT 52, (K,W(K,JM1),W(K,J),WP(K),USTAR(K),SP(K,JM1),SP(K,J),	SCHM1390
1 K=1,NK)	SCHM1400
PRINT 6	SCHM1405
PRINT 52, (I,DHDX(I),DFDX(I),DPDX(I),QPRIM(I),FOLD(I,J),RHOOLD(I,J)	SCHM1410
1 I=1,NCHANL)	SCHM1420
IF(IERROR.GT.1) RETURN	SCHM1425

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450 CONTINUE
IF(JUMP.EQ.3) RETURN
C CORRECT SUBCHANNEL PRESSURES TO ZERO EXIT PRESSURE.
C PRESSURE P(I,J) IS THE PRESSURE ABOVE THE EXIT REFERENCE PRESSURE.
DO 460 I=1,NCHANL
PEXIT = P(I,NDXPI)
DO 460 J=1,NDXPI
460 P(I,J) = P(I,J) - PEXIT
RETURN
END
*DECK HEAT
SURROUTINE HEAT(J)
C CALCULATE THE HEAT INPUT TO EACH SUBCHANNEL AT POSITION J.
C IF NODES GREATER THAN ZERO, CALCULATE HEAT INPUT USING THERMAL
C CONDUCTION. OTHERWISE HEAT INPUT IS DEFINED BY HEAT GENERATION.
C POWER = AVERAGE INTERNAL HEAT GENERATION.
C THIS PROCEDURE CONTAINS THE COMMON AND TYPE STATEMENTS SHARED BY THE
C MAJOR SUBROUTINES OF COBRA-IIIC.
COMMON KIJ, FTM, ABETA, BBETA, AFLUX, Z, THETA, PI, NAX, FLO,
1 GC, I3, I2, NCHANL, NK, IERROR, KDEBUG, NAXL, NGAPS, NGXL,
2 NAFAC, NODES, NSCBC, NRBC, J1, J2, J3, J4, J5, J6, J7,
3 ATOTAL, DX, DT, GK, NV, NF, AV(7), AF(7), QAX, FSPLIT(30)
4 ELEV, NDX, SL, FERROQ, ITERAT, NRAMP, NVISCW, NARAMP
COMMON PP(30), TT(30), VVF(30), VVG(30), HHF(30), HHG(30),
1 UUF(30), KKF(30), SSIGMA(30), NPROP, PREF, TF, VF, VG, HF, HG,
2 UF, KF, SIGMA, HFG, VFG, RHOF, RHOG
COMMON V(30), VP(30), VISC(30), VISCW(30), HFILM(30), CON(30),
1 CP(30), FSP(30), FMULT(30), U(30), UH(30), ALPHA(30), QUAL(30),
2 RHO(30,31), VPA(30), T(30), HINLET(30), FINLET(30)
COMMON COND(47), WP(47), GAP(47), FACTOR(47), IK(47),
1 JK(47), GAPN(47), LENGTH(47), USTAR(47), W(47,31)
COMMON A(30), AN(30), DHYD(30), DHYDN(30), DFOX(30),
1 DHDX(30), DPDX(30), OPRIM(30), PERIM(30),
2 HPERIM(30), NTYPE(30)
COMMON P(30,31), H(30,31), F(30,31), X(31)
COMMON WOLD(47,31), RHOOLD(30,31), FOLD(30,31), HOLD(30,31)
COMMON AXIAL(39), Y(39), IDAPEA(30), IDGAP(47), AA( 4), BB( 4),
1 CC( 4), AFACT(10,10), NCH(10), AXL(10), GAPXL(10), GFACT( 9,10),
2 NGAP( 9), RX(30), XQUAL(30)
COMMON NGRID, NGRIDT, GRIDXL(10), IGRID(10), CD(30, 5),
1 FXFLOW(47, 5), NGTYPE, GRID, FDIV(47)
LOGICAL FDIV, GRID
REAL KIJ, LENGTH, KF, KKF
REAL KFUEL, KCLAD
DIMENSION TDUMY(10)
COMMON /FUEL/ KFUEL( 3), KCLAD( 3), RFUEL( 3), RCLAD( 3),
1 CFUEL( 3), CCLAD( 3), TCLAD( 3), TFLUID,
2 FLUX(35,31), HGAP( 3), TROD(10,35,31), LR(35,6),
3 PARF(30,35), PHI(35,6), RADIAL(35), D(35),
4 POWER, NODESF, NROD, DFUEL( 3), IDFUEL(35), HSURF
NPI = NODESF+1
C BYPASS THE HEAT FLUX CALCULATION IF BEYOND THE FIRST ITERATION AND
C IF FUEL TEMPERATURES ARE NOT TO BE CALCULATED.
IF(ITERAT.GT.1 .AND. NODESF.LT.1) GO TO 60
C BYPASS THE HEAT FLUX CALCULATION USING THE FUEL TEMPERATURE MODEL
C IF BEYOND THE FIRST ITERATION, AND IF FUEL TEMPERATURES HAVE BEEN
C CALCULATED AND IF A TRANSIENT CALCULATION IS BEING PERFORMED.
IF(!ITERAT.GT.1 .AND. NODESF.GT.0 .AND. DT.LT.100.) GO TO 60
CALL CURVE(QAX,(X(J)-DX/2.)/Z,AXIAL,Y,NAX,IERROR,1)

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SCHM1430  
SCHM1440  
SCHM1450  
SCHM1460  
SCHM1470  
SCHM1480  
SCHM1490  
SCHM1500  
SCHM1510  
SCHM1520

HEAT0010  
HEAT0020  
HEAT0030  
HEAT0040  
HEAT0050  
HEAT0060  
HEAT0070  
HEAT0080  
HEAT0090  
HEAT0100  
HEAT0110  
HEAT0120  
HEAT0130  
HEAT0140  
HEAT0150  
HEAT0160  
HEAT0170  
HEAT0180  
HEAT0190  
HEAT0200  
HEAT0210  
HEAT0220  
HEAT0230  
HEAT0240  
HEAT0250  
HEAT0260  
HEAT0270  
HEAT0280  
HEAT0290  
HEAT0300  
HEAT0310  
HEAT0320  
HEAT0330  
HEAT0340  
HEAT0350  
HEAT0360  
HEAT0370  
HEAT0380  
HEAT0390  
HEAT0400  
HEAT0410  
HEAT0420  
HEAT0430  
HEAT0440  
HEAT0450  
HEAT0460  
HEAT0470  
HEAT0480

C	DETERMINE THE HEAT FLUX FROM EACH ROD.	HEAT0490
	DO 50 N=1,NROD	HEAT0500
C	CALCULATE FORCED HEAT FLUX FROM EACH ROD.	HEAT0510
	FLUX(N,J) = AFLUX*RADIAL(N)*QAX*POWER/.0036	HEAT0520
	IF(NODESF.LT.1) GO TO 50	HEAT0530
C	CORRECT HEAT FLUX FOR THERMAL CAPACITY USING TRANSIENT FUEL MODEL.	HEAT0540
C	CALCULATE AVERAGE FLUID TEMPERATURE. HEAT TRANSFER COEFFICIENT.	HEAT0550
	SAVE = 0.	HEAT0560
	TFLUID = 0.	HEAT0570
	HSURF = 0.	HEAT0580
	DO 15 L=1,6	HEAT0590
	IF(LR(N,L)) 15,15,10	HEAT0600
10	I = LR(N,L)	HEAT0610
	DUMY = PHI(N,L)	HEAT0620
	SAVE = SAVE + DUMY	HEAT0630
	TFLUID = TFLUID + T(I)*DUMY	HEAT0640
	HSURF = HSURF + DUMY*HCOOL(N,I,J-1)	HEAT0650
	IF(IEPROR.GT.1) RETURN	HEAT0660
15	CONTINUE	HEAT0670
	IF(SAVE.LE.0.) GO TO 1000	HEAT0680
	TFLUID = TFLUID/SAVE	HEAT0690
	HSURF = HSURF/SAVE	HEAT0700
C		HEAT0710
C	CALCULATE FUEL TEMPERATURE	HEAT0720
	DO 8 I=1,NP1	HEAT0730
8	TDUMY(I) = TROD(I,N,J)	HEAT0740
	CALL TEMP(TDUMY,DT,N,J)	HEAT0750
	IF(IEPROR.GT.1) RETURN	HEAT0760
	DO 17 I=1,NP1	HEAT0770
17	TROD(I,N,J) = TDUMY(I)	HEAT0780
20	FLUX(N,J) = HSURF*(TROD(NP1,N,J) - TFLUID)	HEAT0790
	FLUX(N,J)=AMAX1(0.0,FLUX(N,J))	AEL
50	CONTINUE	HEAT0800
C	CALCULATE HEAT INPUT TO EACH CHANNEL.	HEAT0810
60	DO 100 I=1,NCHANL	HEAT0820
	SAVE = 0.	HEAT0830
	DO 90 N=1,NROD	HEAT0840
	DUMY = PWRP(I,N)	HEAT0850
	IF(DUMY.GT.0.) SAVE = SAVE + DUMY*FLUX(N,J)*PI*D(N)	HEAT0860
90	CONTINUE	HEAT0870
100	QPRIM(I) = SAVE	HEAT0880
	RETURN	HEAT0890
1000	IEPROR = 14	HEAT0900
	RETURN	HEAT0910
	END	HEAT0920
*DECK	TEMP	
	SUBROUTINE TEMP (T,DT,N,JJ)	TEMP0010
C	SUBROUTINE TEMP CALCULATES THE TRANSIENT TEMPERATURE DISTRIBUTION	TEMP0020
C	IN A CYLINDRICAL OR PLATE NUCLEAR FUEL ELEMENT WHERE THE LARGEST	TEMP0030
C	NUMBER NODES IS THE CLADDING. FOR TRANSIENT CALCULATIONS, FLUID	TEMP0040
C	DATA AT T IS USED TO CALCULATE THE TEMPERATURE AT T+DT BY USING	TEMP0050
C	A STABLE IMPLICIT NUMERICAL TECHNIQUE.	TEMP0060
C	SIMULTANEOUS EQUATIONS ARE SOLVED USING A COMPACT ELIMINATION	TEMP0070
C	SCHEME FOR TRI-DIAGONAL MATRICES.	TEMP0080
C		TEMP0090
C	THE VALUE OF T UPON ENTRY IS THE TEMPERATURE AT ORIGINAL TIME.	TEMP0100
C	AT EXIT T IS THE TEMPERATURE DELTA-T LATER IN TIME.	TEMP0110
C		TEMP0120
	COMMON /FUEL/ KFUEL( 3), KCLAD( 3), RFUEL( 3), RCLAD( 3),	TEMP0130

	1 CFUEL( 3), CCLAD( 3), TCLAD( 3), TFLUID,	TEMP0140
	2 FLUX(35,31), HGAP( 3), TROD(10,35,31), LR(35,6),	TEMP0150
	3 PWR( 30,35), PHI(35,6), RADIAL(35), D(35),	TEMP0160
	4 POWER, NODESF, NR0D, DFUEL( 3), IDFUEL(35), H SURF	TEMP0170
	DIMENSION T(10), A(3,10), B(10)	TEMP0180
	REAL KFUEL, KFDR2, KCLAD	TEMP0190
C		TEMP0200
C	SETUP A MATRIX OF THE FORM $A \cdot T = B$ WHERE ONLY THE 3 DIAGONALS OF	TEMP0210
C	A ARE STORED.	TEMP0220
	NM1 = NODESF-1	TEMP0230
	NP1 = NODESF+1	TEMP0240
	IF(NODESF.LE.0) GO TO 1000	TEMP0250
	J = IDFUEL(N)	TEMP0260
	DR = DFUEL(J)*.5/FLOAT(NM1)	TEMP0270
	DR2 = DR**2	TEMP0280
	RCFUEL = RFUEL(J)*CFUEL(J)/DT	TEMP0290
	KFDR2 = KFUEL(J)/DR2	TEMP0300
	HGAP1 = 1./(1./HGAP(J) + TCLAD(J)/KCLAD(J))	TEMP0310
	QCLAD = 0.	TEMP0320
C	J IS THE FUEL TYPE CODE. CYLINDRICAL FUEL, J=1. PLATE FUEL, J=2.	TEMP0330
	IF(J.EQ.2) GO TO 101	TEMP0340
C		TEMP0350
C	THIS SECTION FOR CYLINDERICAL FUEL RODS.	TEMP0360
	QFUEL = FLUX(N,JJ)*4.*D(N)/DFUEL(J)**2	TEMP0370
	DO 100 I=1, NP1	TEMP0380
	IF(I.GT.1) GO TO 10	TEMP0390
	A(2,I) = RCFUEL + 4.*KFDR2	TEMP0400
	A(3,I) = -4.*KFDR2	TEMP0410
	GO TO 80	TEMP0420
	10 IF(I.GT.NM1) GO TO 20	TEMP0430
	A(1,I) = -KFDR2*(1.-1./FLOAT(2*I-2))	TEMP0440
	A(2,I) = RCFUEL + 2.*KFDR2	TEMP0450
	A(3,I) = -KFDR2*(1.+1./FLOAT(2*I-2))	TEMP0460
	GO TO 80	TEMP0470
	20 IF(I.EQ.NP1) GO TO 30	TEMP0480
	A(1,I) = -2.*KFDR2	TEMP0490
	A(2,I) = RCFUEL + 2.*KFDR2 + 2.*HGAP1/DR + HGAP1/DR/FLOAT(I-1)	TEMP0500
	A(3,I) = -(2.*HGAP1/DR + HGAP1/DR/FLOAT(I-1))	TEMP0510
	GO TO 80	TEMP0520
	30 A(1,I) = -HGAP1/TCLAD(J)*DFUEL(J)/D(N)	TEMP0530
	A(2,I) = RCLAD(J)*CCLAD(J)/DT + HGAP1/TCLAD(J)*DFUEL(J)/D(N)	TEMP0540
	+ H SURF/TCLAD(J)	TEMP0550
	80 IF(I.EQ.NP1) GO TO 90	TEMP0560
	B(I) = QFUEL + RCFUEL*T(I)	TEMP0570
	GO TO 100	TEMP0580
	90 B(I) = QCLAD + RCLAD(J)*CCLAD(J)/DT*T(I) + H SURF/TCLAD(J)*TFLUID	TEMP0590
	100 CONTINUE	TEMP0600
C	SOLVE FOR TEMPERATURES	TEMP0610
	CALL GAUSS(1, NP1, A, B, T)	TEMP0620
	RETURN	TEMP0630
C		TEMP0640
C	THIS SECTION FOR FLAT PLATE FUEL.	TEMP0650
	101 QFUEL = FLUX(N,JJ)*2./DFUEL(J)	TEMP0660
	DO 200 I=1, NP1	TEMP0670
	IF(I.GT.1) GO TO 110	TEMP0680
	A(2,I) = RCFUEL + KFDR2*2.	TEMP0690
	A(3,I) = -2.*KFDR2	TEMP0700
	GO TO 180	TEMP0710
	110 IF(I.GT.NM1) GO TO 120	TEMP0720

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A(1,I) = -KFDR2                                TEMP0730
A(2,I) = RCFUEL + 2.*KFDR2                      TEMP0740
A(3,I) = -KFDR2                                TEMP0750
GO TO 180                                       TEMP0760
120 IF(I.EQ.NP1) GO TO 130                       TEMP0770
A(1,I) = -2.*KFDR2                              TEMP0780
A(2,I) = RCFUEL + 2.*KFDR2 + 2.*HGAP1/DR        TEMP0790
A(3,I) = -2.*HGAP1/DR                           TEMP0800
GO TO 180                                       TEMP0810
130 A(1,I) = -HGAP1/TCLAD(J)                     TEMP0820
A(2,I) = RCLAD(J)*CCLAD(J)/DT + HGAP1/TCLAD(J) + HSURF/TCLAD(J) TEMP0830
180 IF(I.EQ.NP1) GO TO 190                       TEMP0840
B(I) = QFUEL + RCFUEL*T(I)                       TEMP0850
GO TO 200                                       TEMP0860
190 B(I) = QCLAD + RCLAD(J)*CCLAD(J)/DT*T(I) + HSURF/TCLAD(J)*TFLUID TEMP0870
200 CONTINUE                                     TEMP0880
C SOLVE FOR TEMPERATURES                        TEMP0890
CALL GAUSS(1,NP1,A,B,T)                          TEMP0900
RETURN                                             TEMP0910
1000 IERROR = 15                                 TEMP0920
RETURN                                             TEMP0930
END                                                TEMP0940
*DECK.HCOOL
FUNCTION HCOOL(N,I,J)                             HCOL0010
C COMPUTES THE HEAT TRANSFER COEFFICIENT FOR ROD N FACING SUBCHANNEL I HCOL0020
C AT AXIAL LOCATION J.                           HCOL0030
C THIS PROCEDURE CONTAINS THE COMMON AND TYPE STATEMENTS SHARED BY THE HCOL0040
C MAJOR SUBROUTINES OF CORRA-IIIC.               HCOL0050
COMMON KIJ, FTM, ABETA, AFLUX, Z, THETA, PI, NAX, FLO, HCOL0060
1 GC, I3, I2, NCHANL, NK, IERROR, KDEBUG, NAXL, NGAPS, NGXL, HCOL0070
2 NAFAC, NODES, NSCBC, NBRC, J1, J2, J3, J4, J5, J6, J7, HCOL0080
3 ATOTAL, DX, DT, GK, NV, NF, AV(7), AF(7), QAX, FSPLIT(30) HCOL0090
4 , ELEV, NDX, SL, FERROR, ITERAT, NRAMP, NVISCV, NARAMP HCOL0100
COMMON PP(30), TT(30), VVF(30), VVG(30), HHF(30), HHG(30), HCOL0110
1 UUF(30), KKF(30), SSIGMA(30), NPROP, PREF, TF, VF, VG, HF, HG, HCOL0120
2 UF, KF, SIGMA, HFG, VFG, RHOF, RHOG HCOL0130
COMMON V(30), VP(30), VISC(30), VISCV(30), HFILM(30), CON(30), HCOL0140
1 CP(30), FSP(30), FMULT(30), U(30), UH(30), ALPHA(30), QUAL(30), HCOL0150
2 PNO(30,31), VPA(30), T(30), HINLET(30), FINLET(30) HCOL0160
COMMON COND(47), WP(47), GAP(47), FACTOR(47), IK(47), HCOL0170
1 JK(47), GAPN(47), LENGTH(47), USTAR(47), W(47,31) HCOL0180
COMMON A(30), AN(30), DHYD(30), DHYDN(30), DFDX(30), HCOL0190
1 DHDX(30), DPOX(30), OPRIM(30), PERIM(30), HCOL0200
2 HPERIM(30), NTYPE(30) HCOL0210
COMMON P(30,31), H(30,31), F(30,31), X(31) HCOL0220
COMMON WOLD(47,31), RHOOLD(30,31), FOLD(30,31), HOLD(30,31) HCOL0230
COMMON AXIAL(39), Y(39), IDAPEA(30), IDGAP(47), AA( 4), RB( 4), HCOL0240
1 CC( 4), AFACT(10,10), NCH(10), AXL(10), GAPXL(10), GFACT( 9,10), HCOL0250
2 NGAP( 9), BX(30), XQUAL(30) HCOL0260
COMMON NGRID, NGRIDT, GRIDXL(10), IGRID(10), CO(30, 5), HCOL0270
1 FXFLOW(47, 5), NGTYPE, GRID, FDIV(47) HCOL0280
LOGICAL FDIV, GRID HCOL0290
REAL KIJ, LENGTH, KF, KKF HCOL0300
C THIS IS ONLY A DUMMY ROUTINE AT THIS TIME PENDING SELECTION OF HCOL0310
C HEAT TRANSFER CORRELATIONS. USERS SHOULD PROVIDE THEIR OWN CORRELATHCOL0320
C HCOOL = SURFACE HEAT TRANSFER COEFFICIENT (BTU/SEC-FT2-F). HCOL0330
REAL KFUEL, KCLAD HCOL0340
COMMON /FUEL/ KFUEL( 3), KCLAD( 3), RFUEL( 3), RCLAD( 3), HCOL0350
1 CFUEL( 3), CCLAD( 3), TCLAD( 3), TFLUID. HCOL0360

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2 FLUX(35,31), HGAP( 3), TROD(10,35,31), LR(35,6),
3 PWRP(30,35), PHI(35,6), RADIAL(35), D(35),
4 POWER, NODESF, NROD, DFUEL( 3), IDFUEL(35), HSURF
IF(NODESF.LE.0) GO TO 1000
HCOOL = 5000./3600.
RETURN
1000 IERROR = 16
RETURN
END
*DECK,CHF
SUBROUTINE CHF(JSTART,JEND)
C CHF SEARCHES COBRA-IIIC OUTPUT AT THE END OF EACH TIME STEP FOR
C THE OCCURANCE OF CRITICAL HEAT FLUX. THE SEARCH IS MADE ON EACH ROD
C AT A SPECIFIED AXIAL LOCATION RANGE BY CONSIDERING EACH ROD AND THE
C ADJACENT CHANNELS.
C ALTHOUGH THE BAW-2 AND W-3 CORRELATIONS ARE INCLUDED, USERS SHOULD
C PROGRAM OTHER CORRELATIONS OF THEIR CHOICE AS OPTIONS.
COMMON KIJ, ABETA, BBETA, AFLUX, Z, THETA, PI, NAX, FLO,
1 GC, I3, I2, NCHANL, NK, IERROR, KDEBUG, NAXL, NGAPS, NGXL,
2 NAFAC, NODES, NSCBC, NARC, J1, J2, J3, J4, J5, J6, J7,
3 ATOTAL, DX, DT, GK, NV, NF, AV(7), AF(7), QAX, FSPLIT(30)
4 ELEV, NDX, SL, FERROR, ITERAT, NRAMP, NVISCW, NARAMP
COMMON PP(30), TT(30), VVF(30), VVG(30), HHF(30), HHG(30),
1 UUF(30), KKF(30), SSIGMA(30), NPROP, PREF, TF, VF, VG, HF, HG,
2 UF, KF, SIGMA, HFG, VFG, RHOF, RHOG
COMMON V(30), VP(30), VISC(30), VISCW(30), HFILM(30), CON(30),
1 CP(30), FSP(30), FMULT(30), U(30), UH(30), ALPHA(30), QUAL(30),
2 RHO(30,31), VPA(30), T(30), HINLET(30), FINLET(30)
COMMON COND(47), WP(47), GAP(47), FACTOR(47), IK(47),
1 JK(47), GAPN(47), LENGTH(47), USTAR(47), W(47,31)
COMMON A(30), AN(30), DHYD(30), DHYDN(30), DFDX(30),
1 DHDX(30), DPDX(30), QPRIM(30), PERIM(30),
2 HPERIM(30), NTYPE(30)
COMMON P(30,31), H(30,31), F(30,31), X(31)
COMMON WOLD(47,31), RHOOLD(30,31), FOLD(30,31), HOLD(30,31)
COMMON AXIAL(39), Y(39), IDAREA(30), IDGAP(47), AA( 4), BB( 4),
1 CC( 4), AFACT(10,10), NCH(10), AXL(10), GAPXL(10), GFACT( 9,10),
2 NGAP( 9), RX(30), XQUAL(30)
COMMON NGRID, NGRIDT, GRIDXL(10), IGRID(10), CD(30, 5),
1 FXFLOW(47, 5), NGTYPE, GRID, FDIV(47)
LOGICAL FDIV, GRID
REAL KIJ, LENGTH, KF, KKF
COMMON /BOIL/ JBOIL(30)
COMMON /FUEL/ KFUEL( 3), KCLAD( 3), RFUEL( 3), RCLAD( 3),
1 CFUEL( 3), CCLAD( 3), TCLAD( 3), TFLUID,
2 FLUX(35,31), HGAP( 3), TROD(10,35,31), LR(35,6),
3 PWRP(30,35), PHI(35,6), RADIAL(35), D(35),
4 POWER, NODESF, NROD, DFUEL( 3), IDFUEL(35), HSURF
COMMON/BCHF/ CHF(35,31), CCHANL(35,31), MCHFR(31), MCHFRC(31),
1 MCHFRR(31), NCHF
INTEGER CCHANL
INTEGER CHFROD
REAL MCHFRR
NDXP1 = NDX + 1
DO 100 J=1,NDXP1
MCHFR(J) = 10.
MCHFRC(J) = 0
MCHFRR(J) = 0
DO 100 N=1,NROD

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HCOL0370
HCOL0380
HCOL0390
HCOL0400
HCOL0410
HCOL0420
HCOL0430
HCOL0440
HCOL0450

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CHF0010
CHF0020
CHF0030
CHF0040
CHF0050
CHF0060
CHF0070
CHF0080
CHF0090
CHF0100
CHF0110
CHF0120
CHF0130
CHF0140
CHF0150
CHF0160
CHF0170
CHF0180
CHF0190
CHF0200
CHF0210
CHF0220
CHF0230
CHF0240
CHF0250
CHF0260
CHF0270
CHF0280
CHF0290
CHF0300
CHF0310
CHF0320
CHF0330
CHF0340
CHF0350
CHF0360
CHF0370
CHF0380
CHF0390
CHF0400
CHF0410
CHF0420
CHF0430
CHF0440
CHF0450
CHF0460
CHF0470
CHF0480
CHF0490

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CHFR(N,J) = 10.	CHF0500
CCHANL(N,J) = 0	CHF0510
100 CONTINUE	CHF0520
DO 500 J=JSTART,JEND	CHF0530
CHFROD = 0	CHF0540
DO 300 N=1,NROD	CHF0550
XMCHFR = 10.	CHF0560
IF (FLUX(N,J).LE.0.) GO TO 300	CHF0570
DO 290 L=1,6	CHF0580
IF (LP(N,L)) 200,290,200	CHF0590
C CALCULATE CHF RATIO FOR ROD N FACING CHANNEL I.	CHF0600
200 I = LP(N,L)	CHF0610
XCHF = 0.	CHF0620
IF (NCHF.EQ.1) XCHF = CHF1(N,I,J)	CHF0630
IF (NCHF.EQ.2) XCHF = CHF2(N,I,J)	CHF0640
IF (XCHF.LE.0.) GO TO 1000	CHF0650
XCHFR = XCHF/FLUX(N,J)	CHF0660
C CALCULATE MINIMUM CHF RATIO FOR ROD N FACING CHANNEL I.	CHF0670
IF (XCHFR.GT.CHFR(N,J)) GO TO 290	CHF0680
CHFR(N,J) = XCHFR	CHF0690
CCHANL(N,J) = I	CHF0700
CHFROD = N	CHF0710
290 CONTINUE	CHF0720
C DETERMINE MINIMUM CHF RATIO AT AXIAL LOCATION J.	CHF0730
XMCHFR = CHFR(N,J)	CHF0740
IF (XMCHFR.GT.MCHFR(J)) GO TO 300	CHF0750
MCHFR(J) = XMCHFR	CHF0760
MCHFR(J) = CHFROD	CHF0770
MCHFR(J) = CCHANL(N,J)	CHF0780
300 CONTINUE	CHF0790
500 CONTINUE	CHF0800
RETURN	CHF0810
1000 PRINT 1	CHF0820
1 FORMAT (' ERROR IN CHF ROUTINE')	CHF0830
RETURN	CHF0840
END	CHF0850
*DECK,CHF1	
FUNCTION CHF1(N,I,J)	CHF10010
COMMON KIJ, FTM, ABETA, BBETA, AFLUX, Z, THETA, PI, NAX, FLO,	CHF10011
1 GC, I3, I2, NCHANL, NK, IERROR, KDEBUG, NAXL, NGAPS, NGXL,	CHF10012
2 NAFAC, NODES, NSCBC, NRRC, J1, J2, J3, J4, J5, J6, J7,	CHF10013
3 ATCTAL, DX, DT, GK, NV, NF, AV(7), AF(7), QAX, FSPLIT(30)	CHF10014
4 , ELFV, NDX, SL, FERROP, ITERAT, NRAMP, NVISCW, NARAMP	CHF10015
COMMON PP(30), TT(30), VVF(30), VVG(30), HHF(30), HHG(30),	CHF10016
1 UUF(30), KKF(30), SSTGMA(30), NPROR, PREF, TF, VF, VG, HF, HG,	CHF10017
2 UF, KF, SIGMA, HFG, VFG, RHO, RHOG	CHF10018
COMMON V(30), VP(30), VISC(30), VISCW(30), HFILM(30), CON(30),	CHF10019
1 CP(30), FSP(30), FMULT(30), U(30), UH(30), ALPHA(30), QUAL(30),	CHF10020
2 RHO(30,31), VPA(30), T(30), HINLET(30), FINLET(30)	CHF10021
COMMON CONN(47), WP(47), GAP(47), FACTOR(47), IK(47),	CHF10022
1 JK(47), GAPN(47), LENGTH(47), USTAR(47), W(47,31)	CHF10023
COMMON A(30), AN(30), DHYD(30), DHYDN(30), DFDX(30),	CHF10024
1 D-DX(30), DPDX(30), OPRIM(30), PERIM(30),	CHF10025
2 HFFILM(30), NTYPE(30)	CHF10026
COMMON P(30,31), H(30,31), F(30,31), X(31)	CHF10027
COMMON KOLD(47,31), RHOOLD(30,31), FOLD(30,31), HOLD(30,31)	CHF10028
COMMON AXIAL(39), Y(39), IDAREA(30), IDGAP(47), AA( 4), BH( 4),	CHF10029
1 CC( 4), AFACT(10,10), NCH(10), AXL(10), GAPXL(10), GFACT( 9,10),	CHF10030
2 NGAP( 9), HX(30), XQUAL(30)	CHF10031

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COMMON NGRID, NGRIDT, GRIDXL(10), IGRID(10), CD(30, 5),
1 FXFLOW(47, 5), NGTYPE, GRID, FDIV(47)
LOGICAL FDIV, GRID
REAL KIJ, LENGTH, KF, KKF, KD
COMMON/ROIL/ JHOIL(30)
COMMON /FUEL/ KFUEL( 3), KCLAD( 3), RFUEL( 3), RCLAD( 3),
1 CFUEL( 3), CCLAD( 3), TCLAD( 3), TFLUID,
2 FLUX(35,31), HGAP( 3), TPOD(10,35,31), LR(35,6),
3 PWRP(30,35), PHI(35,6), RADIAL(35), D(35),
4 POWER, NODESF, NPOD, DFUEL( 3), IDFUEL(35), HSURF
C RAW-2 CHF CORRELATION
DATA A0, B0, A1, A2, A3, A4, A5, A6, A7, A8, A9 / 1.15509, 4.8844,
1 0.3702E+8, 2.1289E-3, 0.83040, 0.68479E-3, 4.5756E+4, 1.0996E-2,
2 0.71186, 0.20729E-3, 547.49/
DATA A21, A22, A23, KD / 2.9840, 7.82293, 0.45758, 1.02506 /
DE = 4.*A(I)/PERIM(I)
XX = (H(I,J)-HF)/HFG
CHF1 = (A0-B0*DE)*(A1*(A2*F(I,J)/A(I))**(A3+A4*(PREF-2000.))
1 - A9*F(I,J)/A(I)*XX*HFG)/(A5*(A6*F(I,J)/A(I))**(A7+A8*(PREF-
2 2000.)))
C AXIAL FLUX CORRECTION FACTOR
FAXIAL = 1.
IF(J.EQ.1) GO TO 10
C = A21*(1.-XX)**A22/(F(I,J)/A(I)*.0036)**A23
SUM = 0.
JS = 2
DO 5 JJ=JS,J
5 SUM = SUM + FLUX(N,JJ)*(EXP(C*X(JJ))-EXP(C*X(JJ-1)))
FAXIAL = SUM*EXP(-C*X(J))/FLUX(N,J)/
1 (1.-EXP(-C*(X(J)-X(JS-1))))*KD
10 CHF1 = CHF1/FAXIAL
RETURN
END
*DECK,CHF2
FUNCTION CHF2(N,I,J)
COMMON KIJ, FTM, ABETA, RBETA, AFLUX, Z, THETA, PI, NAX, FLO,
1 GC, I3, I2, NCHANL, NK, IERROR, KDEBUG, NAXL, NGAPS, NGXL,
2 NAFAC, NODES, NSCBC, NBRC, J1, J2, J3, J4, J5, J6, J7,
3 ATOTAL, DX, DT, GK, NV, NF, AV(7), AF(7), QAX, FSPLIT(30)
4 ELEV, NDX, SL, FERPOR, ITERAT, NRAMP, NVISCW, NARAMP
COMMON PP(30), TT(30), VVF(30), VVG(30), HMF(30), HHG(30),
1 UUF(30), KKF(30), SSIGMA(30), NPROR, PREF, TF, VF, VG, HF, HG,
2 UF, KF, SIGMA, HFG, VFG, RHOF, RHOG
COMMON V(30), VP(30), VISC(30), VISCW(30), HFILM(30), CON(30),
1 CP(30), FSP(30), FMULT(30), U(30), UH(30), ALPHA(30), QUAL(30),
2 RHO(30,31), VPA(30), T(30), HINLET(30), FINLET(30)
COMMON COND(47), WP(47), GAP(47), FACTOR(47), IK(47),
1 JK(47), GAPN(47), LENGTH(47), USTAR(47), W(47,31)
COMMON A(30), AN(30), DHYD(30), DHYDN(30), DFDX(30),
1 DHDX(30), DPDX(30), QPRIM(30), PERIM(30),
2 HPERJM(30), NTYPE(30)
COMMON P(30,31), H(30,31), F(30,31), X(31)
COMMON WOLD(47,31), RHOOLD(30,31), FOLD(30,31), HOLD(30,31)
COMMON AXIAL(39), Y(39), IDAREA(30), IDGAP(47), AA( 4), RR( 4),
1 CC( 4), AFACT(10,10), NCH(10), AXL(10), GAPXL(10), GFACT( 9,10),
2 NGAP( 9), RX(30), XQUAL(30)
COMMON NGRID, NGRIDT, GRIDXL(10), IGRID(10), CD(30, 5),
1 FXFLOW(47, 5), NGTYPE, GRID, FDIV(47)
LOGICAL FDIV, GRID
CHF10032
CHF10033
CHF10034
CHF10035
CHF10036
CHF10037
CHF10038
CHF10039
CHF10040
CHF10041
CHF10042
CHF10043
CHF10044
CHF10050
CHF10070
CHF10080
CHF10090
CHF10100
CHF10110
CHF10120
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CHF10170
CHF10180
CHF10190
CHF10200
CHF10210
CHF10220
CHF10230
CHF10240
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CHF20027
CHF20028
CHF20029
CHF20030
CHF20031
CHF20032
CHF20033
CHF20034

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REAL KIJ, LENGTH, KF, KKF
COMMON /HOIL/ JHOIL(30)
COMMON /FUFL/ KFUEL( 3), KCLAD( 3), RFUEL( 3), RCLAD( 3),
1 CFUEL( 3), CCLAD( 3), TCLAD( 3), TFLUID,
2 FLUX(35,31), HGAP( 3), THOJ(10,35,31), LR(35,6),
3 PWRP(30,35), PHI(35,6), RADIAL(35), D(35),
4 POWER, NODSF, NPOD, DFUEL( 3), IDFUEL(35), HSURF
C W-3 CORRELATION INCLUDING, SPACER FACTOR, UNHEATED WALL CORRECTION. CHF20035
C AXIAL FLUX FACTOR CHF20036
C REFERENCE, LS TONG, BOILING CRISIS AND CRITICAL HEAT FLUX CHF20037
C AEC CRITICAL REVIEW SERIES, TID-25887(1972). CHF20038
DE = 4.*A(I)/PERIM(I) CHF20039
DH = 4.*A(I)/HPERIM(I) CHF20040
RU = 1.-DE/DH CHF20041
XX = (H(I,J)-HF)/HFG CHF20042
C W-3 CORRELATION USING EQUILIBRIUM STEAM QUALITY CHF20043
CHF2 = ((2.022 - 0.0004302*PREF) + (0.1722 - 0.0000984*PREF) CHF20044
1 *EXP((18.2 - 0.004129*PREF)*XX)) CHF20045
2 *((0.1484 - 1.596*XX + 0.1729*XX*ABS(XX))*F(I,J)/A(I) CHF20046
3 *.0036 + 1.037) CHF20047
4 *(1.157 - 0.869*XX) CHF20048
5 *(0.2664 + 0.8357*EXP(-37.812*DH)) CHF20049
6 *(0.8258 + 0.000794*(HF-HINLFT(I)))/.0036 CHF20050
C UNHEATED WALL CORRECTION CHF20051
IF(RU.GT.0.) CHF2 = CHF2*(1. - RU*(13.76-1.372*EXP(1.78*XX) CHF20052
1-4.732/(F(I,J)/A(I)*.0036)**.0575-.619*(PREF/1000)**.14 CHF20053
2-102.11*DH**.107)) CHF20054
C SPACER FACTOR CORRECTION CHF20055
C USER SHOULD SELECT PROPER VALUE OF TDC CHF20056
TDC = .000 CHF20057
IF(NGRID.GT.0) CHF2 = CHF2 CHF20058
1*(1.0 + 0.03*F(I,J)/A(I)*.0036 * (TDC/0.019)**.35) CHF20059
C AXIAL FLUX PROFILE CORRECTION CHF20060
FAXIAL = 1. CHF20061
IF(J.LE.JHOIL(I)) GO TO 10 CHF20062
C = 1.8*(1.-XX)**4.31/(F(I,J)/A(I)*.0036)**.478 CHF20063
SUM = 0. CHF20064
JS = JHOIL(I)+1 CHF20065
DO 5 JJ=JS,J CHF20066
5 SUM = SUM + FLUX(N, JJ)*(EXP(C*X(JJ))-EXP(C*X(JJ-1))) CHF20067
FAXIAL = SUM*EXP(-C*X(J))/FLUX(N,J)/ CHF20068
1 (1.-EXP(-C*(X(J)-X(JS-1)))) CHF20069
10 CHF2 = CHF2/FAXIAL CHF20070
RETURN CHF20071
END CHF20072
*DECK, GAUSS
SUBROUTINE GAUSS (N,M,A,B,T) GAUS0010
C SUBROUTINE SOLVES TRIDIAGONAL MATRIX BY GAUSS ELIMINATION GAUS0020
DIMENSION A(3,10), B(10), T(10) GAUS0030
MM = M-1 GAUS0040
DO 10 K = N,MM GAUS0050
AK = A(1,K+1)/A(2,K) GAUS0060
A(2,K+1) = A(2,K+1)-A(3,K)*AK GAUS0070
10 B(K+1) = B(K+1)-B(K)*AK GAUS0080
T(M) = B(M)/A(2,M) GAUS0090
DO 20 K = N,MM GAUS0100
L = MM-K+N GAUS0110
20 T(L) = (B(L)-A(3,L)*T(L+1))/A(2,L) GAUS0120
RETURN GAUS0130

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END
*DECK,DIFFER
SUBROUTINE DIFFER(IPART,J)
C THIS PROCEDURE CONTAINS THE COMMON AND TYPE STATEMENTS SHARED BY THE
C MAJOR SUBROUTINES OF CORRA-IIIC.
COMMON KIJ, FTM, ABETA, BBETA, AFLUX, Z, THETA, PI, NAX, FLO,
1 GC, I3, I2, NCHANL, NK, IERROR, KDEBUG, NAXL, NGAPS, NGXL,
2 NAFAC, NODES, NSCBC, NRRC, J1, J2, J3, J4, J5, J6, J7,
3 ATOTAL, DX, DT, GK, NV, NF, AV(7), AF(7), QAX, FSPLIT(30)
4 , ELEV, NDX, SL, FERROP, ITERAT, NRAMP, NVISW, NARAMP
COMMON PP(30), TT(30), VVF(30), VVG(30), HHF(30), HHG(30),
1 UUF(30), KKF(30), SSIGMA(30), NPROP, PREF, TF, VF, VG, HF, HG,
2 UF, KF, SIGMA, HFG, VFG, RHO, RHOG
COMMON V(30), VP(30), VISC(30), VISCW(30), HFILM(30), CON(30),
1 CP(30), FSP(30), FMULT(30), U(30), UH(30), ALPHA(30), QUAL(30),
2 RHO(30,31), VPA(30), T(30), HINLET(30), FINLET(30)
COMMON COND(47), WP(47), GAP(47), FACTOR(47), IK(47),
1 JK(47), GAPN(47), LENGTH(47), USTAR(47), W(47,31)
COMMON A(30), AN(30), DHYD(30), DHYDN(30), DFDX(30),
1 DHDX(30), DPDX(30), QPRIM(30), PERIM(30),
2 HPERIM(30), NTYPE(30)
COMMON P(30,31), H(30,31), F(30,31), X(31)
COMMON WOLD(47,31), RHOOLD(30,31), FOLD(30,31), HOLD(30,31)
COMMON AXIAL(39), Y(39), IDAREA(30), IDGAP(47), AA( 4), RB( 4),
1 CC( 4), AFACT(10,10), NCH(10), AXL(10), GAPXL(10), GFACT( 9,10),
2 NGAP( 9), BX(30), XQUAL(30)
COMMON NGRID, NGRIDT, GRIDXL(10), IGRID(10), CD(30, 5),
1 FXFLOW(47, 5), NGTYPE, GRID, FDIV(47)
LOGICAL FDIV, GRID
REAL KIJ, LENGTH, KF, KKF
COMMON /DP/ DPK(30)
JMI = J-1
NKK = NK
NCHAN = NCHANL
IF(IPART.LT.1 .OR. IPART.GT.4) GO TO 1000
GO TO (100,200,300,400).IPART
C
C PART 1. CALCULATE DH/DX FOR STEADY STATE AT X AND T.
CC IF(J.EQ.1) FLOWSQ = F(I,1)**2
100 DO 190 I=1,NCHAN
SAVE = 0.
DO 170 K=1,NKK
SKI = S(K,I)
IF(SKI) 120,170,120
120 II = IK(K)
JJ = JK(K)
HSTAR = H(II,J)
IF(W(K,J).LT.0.) HSTAR = H(JJ,J)
DUMY = SKI*((H(JJ,J)-H(II,J))*WP(K) + (H(I,J)-HSTAR)*W(K,J)
1 + (T(JJ)-T(II))*COND(K))
SAVE = SAVE + DUMY
170 CONTINUE
DHDX(I) = (SAVE + QPRIM(I))/F(I,J)
170 CONTINUE
GO TO 500
C
C PART 2. CALCULATE DF/DX FOR STEADY STATE AT X AND T
200 DO 290 I=1,NCHAN
SAVE = 0.

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GAUS0140

DIFF0010  
DIFF0020  
DIFF0030  
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DIFF0050  
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DIFF0540  
DIFF0550  
DIFF0560

DO 270 K=1,NKK	DIFF0570
IF(S(K,I)) 220,270,230	DIFF0580
220 SAVE = SAVE + W(K,J)	DIFF0590
GO TO 270	DIFF0600
230 SAVE = SAVE - W(K,J)	DIFF0610
270 CONTINUE	DIFF0620
DPDX(I) = SAVE	DIFF0630
290 CONTINUE	DIFF0640
GO TO 500	DIFF0650
C	DIFF0660
C PART 3. CALCULATE DP/DX WITHOUT W	DIFF0670
300 DO 390 I=1,NCHAN	DIFF0680
SAVE = .5*FSP(I)*FMULT(I)*V(I)/DHVD(I)	DIFF0690
1 + (VP(I)/A(I)-VPA(I))*A(I)/DX	DIFF0700
IF(.NOT.GRID) GO TO 310	DIFF0710
IF(NRAMP.LE.0) GO TO 1000	DIFF0720
DUMY = FLOAT(ITERAT)/FLOAT(NRAMP)	DIFF0730
IF(DUMY.GT.1.) DUMY = 1.	DIFF0740
SAVE = SAVE + .5*DUMY*CD(I,NGTYPE)*VP(I)/DX	DIFF0750
310 DPK(I) = SAVE/A(I)/A(I)	DIFF0760
DUMY = 0.	DIFF0770
IF(FTM.LE.0.) GO TO 380	DIFF0780
DO 370 K=1,NKK	DIFF0790
SKI = S(K,I)	DIFF0800
IF(SKI) 320,370,320	DIFF0810
320 II = IK(K)	DIFF0820
JJ = JK(K)	DIFF0830
DUMY = DUMY + SKI*(U(II)-U(JJ))*WP(K)	DIFF0840
370 CONTINUE	DIFF0850
380 FLOWSQ = ABS(F(I,JM1))*F(I,JM1)	DIFF0860
IF(J.EQ.1) FLOWSQ = F(I,1)**2	DIFF0865
DPDX(I) = -DPK(I)*FLOWSQ/GC	DIFF0870
1 - RHO(I,J)*ELEV - DUMY/A(I)/GC*FTM	DIFF0880
IF(DT.GT.100.) GO TO 390	DIFF0900
RHODOT = (RHO(I,J)-RHOOLD(I,J))/DT	DIFF0910
DPDX(I) = DPDX(I) + RHODOT/GC*(2.*U(I)+DX/DT	DIFF0920
1 + DPK(I)*ABS(F(I,JM1)+F(I,J))*A(I)*DX)	DIFF0930
2 + (FOLD(I,J)-F(I,JM1))/A(I)/DT/GC	DIFF0940
390 CONTINUE	DIFF0950
GO TO 500	DIFF0960
C	DIFF0970
C PART 4. CALCULATE DP/DX WITH W	DIFF0980
400 DO 490 I=1,NCHAN	DIFF0990
DUMY = 0.	DIFF1000
IF(J.EQ.1) GO TO 480	DIFF1010
DO 470 K=1,NKK	DIFF1020
IF(S(K,I)) 420,470,430	DIFF1030
420 DUMY = DUMY + ((2.*U(I)-USTAR(K)+DX/DT)/A(I)	DIFF1040
1 + DPK(I)*ABS(F(I,JM1)+F(I,J))*DX)*W(K,J)	DIFF1050
GO TO 470	DIFF1060
430 DUMY = DUMY - ((2.*U(I)-USTAR(K)+DX/DT)/A(I)	DIFF1070
1 + DPK(I)*ABS(F(I,JM1)+F(I,J))*DX)*W(K,J)	DIFF1080
470 CONTINUE	DIFF1090
480 DPDX(I) = DPDX(I) - DUMY/GC	DIFF1100
490 CONTINUE	DIFF1110
500 RETURN	DIFF1120
1000 IFFROR = 2	DIFF1130
RETURN	DIFF1140
END	DIFF1150

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*DECK, DIVERT
SUBROUTINE DIVERT(J)
C THIS PROCEDURE CONTAINS THE COMMON AND TYPE STATEMENTS SHARED BY THE
C MAJOR SUBROUTINES OF CORWA-IIIC.
COMMON KIJ, FTM, ABETA, BBETA, AFLUX, Z, THETA, PI, NAX, FLO,
1 GC, I3, I2, NCHANL, NK, IERPOR, KDEBUG, NAXL, NGAPS, NGXL,
2 NAFAC, NODES, NSCRC, NBRC, J1, J2, J3, J4, J5, J6, J7,
3 ATOTAL, DX, DT, GK, NV, NF, AV(7), AF(7), QAX, FSPLIT(30)
4 ELEV, NDX, SL, FERROW, ITERAT, NRAMP, NVISCW, NARAMP
COMMON PP(30), TT(30), VVF(30), VVG(30), HHF(30), HHG(30),
1 UUF(30), KKF(30), SSIGMA(30), NPROP, PREF, TF, VF, VG, HF, HG,
2 UF, KF, SIGMA, HFG, VFG, RHOF, RHOG
COMMON V(30), VP(30), VISC(30), VISCW(30), HFILM(30), CON(30),
1 CP(30), FSP(30), FMULT(30), U(30), UH(30), ALPHA(30), QUAL(30),
2 RHO(30,31), VPA(30), T(30), HINLET(30), FINLET(30)
COMMON COND(47), WP(47), GAP(47), FACTOR(47), IK(47),
1 JK(47), GAPN(47), LENGTH(47), USTAR(47), W(47,31)
COMMON A(30), AN(30), DHYD(30), DHYDN(30), DFDX(30),
1 DHDX(30), DPDX(30), QPRIM(30), PERIM(30),
2 HPERIM(30), NTYPE(30)
COMMON P(30,31), H(30,31), F(30,31), X(31)
COMMON WOLD(47,31), RHOOLD(30,31), FOLD(30,31), HOLD(30,31)
COMMON AXIAL(39), Y(39), IDAREA(30), IDGAP(47), AA( 4), BB( 4),
1 CC( 4), AFACT(10,10), NCH(10), AXL(10), GAPXL(10), GFACT( 9,10),
2 NGAP( 9), BX(30), XQUAL(30)
COMMON NGRID, NGRIDT, GRIDXL(10), IGRID(10), CD(30, 5),
1 FXFLOW(47, 5), NGTYPE, GRID, FDIV(47)
LOGICAL FDIV, GRID
REAL KIJ, LENGTH, KF, KKF
COMMON /BUL/ AAA(47,47), ANSWER(47), B(47), IPS(47)
COMMON /BSP/ SP(47,31)
COMMON /DP/ DPK(30)
DIMENSION USAVE(47)
NKK = NK
NCHAN = NCHANL
JMI = J-1
SLDX = SL*DX
DTGC = DT*GC
DXGC = DX*GC
C CALCULATE USTAR
DO 5 K=1,NKK
II = IK(K)
JJ = JK(K)
USAVE(K) = USTAR(K)
USTAR(K) = .5*(U(II)+U(JJ))
5 CONTINUE
C SET UP THE SIMULTANEOUS EQUATIONS
DO 40 K=1,NKK
DO 40 L=1,NKK
SAVE = 0.
DO 50 I=1,NCHAN
IF(S(K,I)) 10,50,20
10 IF(S(L,I)) 30,50,40
20 IF(S(L,I)) 40,50,30
30 SAVE = SAVE + (2.*U(I)-USTAR(L)+DX/DT)/A(I)
I + DPK(I)*ABS(F(I,JMI)+F(I,J))*DX
GO TO 50
40 SAVE = SAVE - (2.*U(I)-USTAR(L)+DX/DT)/A(I)
I - DPK(I)*ABS(F(I,JMI)+F(I,J))*DX

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50	CONTINUE	DVRT0590
	AAA(K,L) = SAVE*SLDX/GC*FACTOR(L)	DVRT0600
60	CONTINUE	DVRT0610
	II = IK(K)	DVRT0620
	JJ = JK(K)	DVRT0630
	R(K) = (SP(K,J) - (DPDX(II)-DPDX(JJ))*DX)*SL*FACTOR(K)	DVRT0640
	1 + USAVE(K)*W(K,JM1)/DXGC + WOLD(K,J)/DTGC	DVRT0650
	AAA(K,K) = AAA(K,K) + SL*CIJ(K,J)*FACTOR(K)	DVRT0660
	1 + USTAR(K)/DXGC + 1./DTGC	DVRT0670
40	CONTINUE	DVRT0680
	IF(J6.LT.1) GO TO 105	DVRT0690
C		DVRT0700
C	MODIFY SIMULTANEOUS EQUATIONS TO ACCOUNT FOR SPECIFIED VALUES OF	DVRT0710
C	CROSSFLOW GIVEN IN SUBROUTINE FORCE	DVRT0720
C		DVRT0730
	DO 90 K=1,NK	DVRT0740
	IF(FDIV(K)) GO TO 90	DVRT0750
	DO 85 L=1,NK	DVRT0760
	IF(L.EQ.K) GO TO 85	DVRT0770
	IF(FDIV(L)) B(K) = B(K) - AAA(K,L)*W(L,J)	DVRT0780
85	CONTINUE	DVRT0790
90	CONTINUE	DVRT0800
	DO 100 K=1,NK	DVRT0810
	IF(.NOT.FDIV(K)) GO TO 100	DVRT0820
	DO 95 L=1,NK	DVRT0830
	AAA(K,L) = 0.	DVRT0840
95	AAA(L,K) = 0.	DVRT0850
	AAA(K,K) = 1.	DVRT0860
	B(K) = W(K,J)	DVRT0870
100	CONTINUE	DVRT0880
105	IF(KDEBUG.LT.1) GO TO 110	DVRT0890
	PRINT 2, ((AAA(K,L),L=1,NKK),B(K),K=1,NKK)	DVRT0900
	2 FORMAT(7E14.7)	DVRT0910
110	CALL DECOMP(NKK,IERROR)	DVRT0920
	IF(IERROR.GT.1) GO TO 1000	DVRT0930
	CALL SOLVE(NKK)	DVRT0940
	DO 150 K=1,NKK	DVRT0950
150	W(K,J) = ANSWER(K)	DVRT0960
	RETURN	DVRT0970
1000	PRINT 1	DVRT0980
	1 FORMAT(24H ERROR IN DECOMP, DIVERT )	DVRT0990
	IERROR = 3	DVRT1000
	RETURN	DVRT1010
	END	DVRT1020
*DECK.PROP		
	SUBROUTINE PROP(IPART,J)	PROP0010
C	THIS PROCEDURE CONTAINS THE COMMON AND TYPE STATEMENTS SHARED BY THE	PROP0020
C	MAJOR SUBROUTINES OF COBRA-IIIC.	PROP0030
	COMMON KIJ, FTM, ABETA, BBETA, AFLUX, Z, THETA, PI, NAX, FLO,	PROP0040
	1 GC, I3, I2, NCHANL, NK, IERROR, KDEBUG, NAXL, NGAPS, NGXL,	PROP0050
	2 NAFAC, NODES, NSCBC, NARC, J1, J2, J3, J4, J5, J6, J7,	PROP0060
	3 ATOTAL, DX, DT, GK, NV, NF, AV(7), AF(7), QAX, FSPLIT(30)	PROP0070
	4 , ELEV, NDX, SL, FERPOR, ITERAT, NRAMP, NVISCW, NARAMP	PROP0080
	COMMON PP(30), TT(30), VVF(30), VVG(30), HHF(30), HHG(30),	PROP0090
	1 UHF(30), KKF(30), SSIGMA(30), NPROP, PREF, TF, VF, VG, HF, HG,	PROP0100
	2 UF, KF, SIGMA, HFG, VFG, RHOF, RHOG	PROP0110
	COMMON V(30), VP(30), VISC(30), VISCW(30), HFILM(30), CON(30),	PROP0120
	1 CP(30), FSP(30), FMULT(30), U(30), UH(30), ALPHA(30), QUAL(30),	PROP0130
	2 RHO(30,31), VPA(30), T(30), MINLET(30), FINLET(30)	PROP0140

COMMON COND(47), WP(47), GAP(47), FACTOR(47), IK(47),	PROP0150
1 JK(47), GAPN(47), LENGH(47), USTAR(47), W(47,31)	PROP0160
COMMON A(30), AN(30), DHYD(30), DHYDN(30), DFOX(30),	PROP0170
1 DDPX(30), DDPX(30), OPRIM(30), PERIM(30),	PROP0180
2 HPERJM(30), NTYPE(30)	PROP0190
COMMON P(30,31), H(30,31), F(30,31), X(31)	PROP0200
COMMON WOLD(47,31), RHOOLD(30,31), FOLD(30,31), HOLD(30,31)	PROP0210
COMMON AXIAL(39), Y(39), IDAREA(30), IDGAP(47), AA( 4), RB( 4),	PROP0220
1 CC( 4), AFACT(10,10), NCH(10), AXL(10), GAPXL(10), GFACT( 9,10),	PROP0230
2 NGAP( 9), BX(30), XQHIAL(30)	PROP0240
COMMON NGRID, NGRIDT, GRIDXL(10), IGRID(10), CD(30, 5),	PROP0250
1 FXFLOW(47, 5), NGTYPE, GRID, FDIV(47)	PROP0260
LOGICAL FDIV, GRID	PROP0270
REAL KIJ, LENGTH, KF, KKF	PROP0280
COMMON /BOIL/ JBOIL(30)	PROP0285
1 FORMAT(28H REYNOLDS NUMBER IN CHANNEL ,I2,19H IS TOO LOW. RE = ,	PROP0290
1 E10.4 )	PROP0300
5 FORMAT(50H FAILURE OF SUBROUTINE PROP, PRESSURE TOO LOW FOR TABLE	PROP0310
1P = E12.5 /(10E10.4))	PROP0320
6 FORMAT(61H FAILURE OF SUBROUTINE PROP, PRESSURE TOO HIGH FOR TABLE	PROP0330
1P = E12.5 /(10E10.4))	PROP0340
7 FORMAT(40H TABLE LOOKUP FAILED IN SUBROUTINE PROP . )	PROP0350
NPROP = NPROP	PROP0360
IF(IPART.LT.1 .OR. IPART.GT.2) GO TO 1001	PROP0370
GO TO (9,100),IPART	PROP0380
C	PROP0390
C PART 1. CALCULATION OF SATURATED PROPERTIES	PROP0400
9 DO 10 I=1,NPROP	PROP0410
IF(PREF.LT.PP(I)) GO TO 20	PROP0420
10 CONTINUE	PROP0430
GO TO 200	PROP0440
20 IF(I.GT.1) GO TO 40	PROP0450
GO TO 210	PROP0460
40 VALUE = (PREF-PP(I-1))/(PP(I)-PP(I-1))	PROP0470
HF = HHF(I-1) + VALUE*( HHF(I)- HHF(I-1))	PROP0480
HG = HHG(I-1) + VALUE*( HHG(I)- HHG(I-1))	PROP0490
VF = VVF(I-1) + VALUE*( VVF(I)- VVF(I-1))	PROP0500
VG = VVG(I-1) + VALUE*( VVG(I)- VVG(I-1))	PROP0510
UF = UUF(I-1) + VALUE*( UUF(I)- UUF(I-1))	PROP0520
TF = TT(I-1) + VALUE*( TT(I)- TT(I-1))	PROP0530
KF = KKF(I-1) + VALUE*( KKF(I)- KKF(I-1))	PROP0540
SIGMA = SSIGMA(I-1) + VALUE*(SSIGMA(I)-SSIGMA(I-1))	PROP0550
HFG = HG-HF	PROP0560
VFG = VG-VF	PROP0570
RHOG = 1./VG	PROP0580
RHOF = 1./VF	PROP0590
RETURN	PROP0600
C	PROP0610
C PART 2. CALCULATE LIQUID PROPERTIES AND PARAMETERS	PROP0620
100 NCHAN = NCHANL	PROP0630
IF(J.GT.1) GO TO 102	PROP0640
DO 101 I=1,NCHAN	PROP0644
101 JBOIL(I) = 0	PROP0645
102 DO 150 J=1,NCHAN	PROP0646
VISCW(I) = UF	PROP0650
VISC(J) = UF	PROP0660
T(I) = TF	PROP0670
CON(I) = KF	PROP0680
V(I) = VF	PROP0690

HH = H(I,J)	PROP0700
IF(HH.GT.HF) GO TO 105	PROP0710
CALL CURVE (VISC(I),HH,UUF,HMF,NPROP,IERROR,1)	PROP0720
IF(IERROR.GT.1) GO TO 1000	PROP0730
CALL CURVE (V(I),HH,VVF,HMF,NPROP,IERROR,2)	PROP0740
CALL CURVE (T(I),HH,TT,HMF,NPROP,IERROR,2)	PROP0750
CALL CURVE (CON(I),HH,KKF,HMF,NPROP,IERROR,2)	PROP0760
105 TM = T(I)-1.	PROP0770
CALL CURVE (HM,TM,HMF,TT,NPROP,IERROR,1)	PROP0780
IF(IERROR.GT.1) GO TO 1000	PROP0790
CP(I) = HH-HM	PROP0800
IF(HH.GT.HF) CP(I) = HF-HM	PROP0810
VISC(I) = VISC(I)/3600.	PROP0820
CON(I) = CON(I)/3600.	PROP0840
RE = F(I,J)/A(I)*DHYD(I)/VISC(I)	PROP0850
IF(RE.LT.0.) PRINT 1, I, RE	PROP0860
IF(RE.LT.2000.) RE = 2000.	PROP0870
PR = CP(I)*VISC(I)/CON(I)	PROP0880
IF(H(I,J).GT.HF) GO TO 120	PROP0890
HFILM(I) = 0.023*CON(I)/DHYD(I)*RE**.8*PR**.4	PROP0900
DTWALL = QPRIM(I)/HPERIM(I)/HFILM(I)	PROP0910
C DETERMINE THE START OF NUCLEATE BOILING	PROP0920
IF(JBOIL(I).GT.0) GO TO 110	PROP0930
TLBOIL = TF - DTWALL + 60.*EXP(-PREF/900.)*(QPRIM(I)/HPERIM(I)	PROP0940
1 *.0036)**.25	PROP0941
IF(T(I).GE.TLBOIL) JBOIL(I) = J	PROP0945
110 TWALL = T(I) + DTWALL	PROP0946
IF(TWALL.LT.TF) CALL CURVE(VISCW(I),TWALL,UUF,TT,NPROP,IERROR,1)	PROP0947
IF(IERROR.GT.1) GO TO 1000	PROP0950
120 L = NTYPE(I)	PROP0970
FSP(I) = AA(L)*RE**BR(L)+CC(L)	PROP0980
VISCW(I) = VISCW(I)/3600.	PROP0985
IF(NVISCW.EQ.1)	PROP0990
FSP(I) = FSP(I)*(1.+HPERIM(I)/PERIM(I)*((VISCW(I)/VISC(I))**.6-1.))	PROP1005
150 CONTINUE	PROP1010
RETURN	PROP1020
200 WRITE(I3,6) PREF,PP	PROP1030
GO TO 1001	PROP1040
210 WRITE(I3,5) PREF,PP	PROP1050
GO TO 1001	PROP1060
1000 WRITE(I3,7)	PROP1070
1001 IERROR = 11	PROP1080
RETURN	PROP1090
END	PROP1100
*DECK,VOID	
SUBROUTINE VOID (J)	VOID0010
COMMON KIJ, FTM, ABETA, BBETA, AFLUX, Z, THETA, PI, NAX, FLO,	VOID0020
1 GC, I3, I2, NCHANL, NK, IERROR, KDEBUG, NAXL, NGAPS, NGXL,	VOID0030
2 NAFAC, NODES, NSCBC, NBRC, J1, J2, J3, J4, J5, J6, J7,	VOID0040
3 ATOTAL, DX, DT, GK, NV, NF, AV(7), AF(7), QAX, FSPLIT(30)	VOID0050
4 . ELEV, NDX, SL, FERROR, ITERAT, NRAMP, NVISCW, NARAMP	VOID0060
COMMON PP(30), TT(30), VVF(30), VVG(30), HMF(30), MHG(30),	VOID0070
1 UUF(30), KKF(30), SSIGMA(30), NPROP, PREF, TF, VF, VG, HF, HG,	VOID0080
2 UF, KF, SIGMA, HFG, VFG, RHOF, RHOG	VOID0090
COMMON V(30), VP(30), VISC(30), VISCW(30), HFILM(30), CON(30),	VOID0100
1 CP(30), FSP(30), FMULT(30), U(30), UM(30), ALPHA(30), QUAL(30),	VOID0110
2 RHO(30,31), VPA(30), T(30), HINLET(30), FINLET(30)	VOID0120
COMMON COND(47), WP(47), GAP(47), FACTOR(47), IK(47),	VOID0130
1 JK(47), GAPN(47), LENGTH(47), USTAR(47), W(47,31)	VOID0140

COMMON A(30), AN(30), DHYD(30), DHYDN(30), DFDX(30),	VOID0150
1 DMHX(30), DPDX(30), QPRIM(30), PERIM(30),	VOID0160
2 HPEWIM(30), NTYPE(30)	VOID0170
COMMON P(30,31), H(30,31), F(30,31), X(31)	VOID0180
COMMON WOLD(47,31), RHOLD(30,31), FOLD(30,31), HOLD(30,31)	VOID0190
COMMON AXIAL(39), Y(39), IDAPEA(30), IDGAP(47), AA( 4), BB( 4),	VOID0200
1 CC( 4), AFACT(10,10), NCH(10), AXL(10), GAPXL(10), GFACT( 9,10),	VOID0210
2 NGAP( 9), HX(30), XQUAL(30)	VOID0220
COMMON NGRID, NGRIDT, GRIDXL(10), IGRID(10), CD(30, 5),	VOID0230
1 FXFLOW(47, 5), NGTYPE, GRID, FDIV(47)	VOID0240
LOGICAL FDIV, GRID	VOID0250
REAL KIJ, LENGTH, KF, KKF	VOID0260
DIMENSION PHI(30)	VOID0270
EQUIVALENCE (FMULT(1),PHI(1))	VOID0280
NCHAN = NCHANL	VOID0290
DO 200 I=1,NCHAN	VOID0300
PSI = 0.	VOID0310
DPSIDH = 0.	VOID0320
IF(J3.EQ.0) GO TO 40	VOID0330
H(I,J) = H(I,J) - .1	VOID0340
QUAL(I) = (H(I,J)-HF)/HFG	VOID0350
IF(J2.EQ.1) QUAL(I) = SCQUAL(I,J)	VOID0360
IF(QUAL(I).LE.0.) QUAL(I) = 0.	VOID0370
ALPHA(I) = RVOID(I,J)	VOID0380
PSI = RHOF*QUAL(I)*(1.-ALPHA(I))-RHOG*ALPHA(I)*(1.-QUAL(I))	VOID0390
H(I,J) = H(I,J) + .1	VOID0400
40 QUAL(I) = (H(I,J)-HF)/HFG	VOID0410
IF(J2.EQ.1) QUAL(I) = SCQUAL(I,J)	VOID0420
IF(QUAL(I).LE.0.) GO TO 150	VOID0430
XP = QUAL(I)	VOID0440
ALPHA(I) = RVOID(I,J)	VOID0450
C CALCULATE TWO-PHASE DENSITY.	VOID0460
RHO(I,J) = RHOG*ALPHA(I)+RHOF*(1.-ALPHA(I))	VOID0470
C CALCULATE TWO-PHASE SPECIFIC VOLUME FOR MOMENTUM.	VOID0480
VP(I) = VF*(1.-XP)**2/(1.-ALPHA(I))+VG*XP**2/ALPHA(I)	VOID0490
C TWO-PHASE FRICTIONAL PRESSURE GRADIENT MULTIPLIERS.	VOID0500
PHI(I) = 1.	VOID0510
IF(J4.EQ.0) PHI(I) = RHOF/RHO(I,J)	VOID0520
IF(J4.NE.1) GO TO 50	VOID0530
PHI(I) = 1.	VOID0540
IF(ALPHA(I).GT.0..AND.ALPHA(I).LE..6) PHI(I)=(1.-XP)**2/(1.-	VOID0550
1 ALPHA(I))**1.42	VOID0560
IF(ALPHA(I).GT..6.AND.ALPHA(I).LE..9) PHI(I)= .478*(1.-XP)**2/	VOID0570
1 (1.-ALPHA(I))**2.2	VOID0580
IF(ALPHA(I).GT..9.AND.ALPHA(I).LE.1.) PHI(I)= 1.73*(1.-XP)**2/	VOID0590
1 (1.-ALPHA(I))**1.64	VOID0600
50 IF(J4.NE.5) GO TO 140	VOID0610
PHI(I) = AF(I)	VOID0620
XX = QUAL(I)	VOID0630
DO 130 K=2,NF	VOID0640
PHI(I) = PHI(I)+AF(K)*XX	VOID0650
130 XX = XX*QUAL(I)	VOID0660
140 U(I) = F(I,J)/A(I)*VP(I)	VOID0670
IF(J3.EQ.0) GO TO 145	VOID0680
DPSIDH = -10.*(PSI-RHOF*QUAL(I)*(1.-ALPHA(I))+RHOG*ALPHA(I)*	VOID0690
1 (1.-QUAL(I)))	VOID0700
145 U(I) = F(I,J)/A(I)/(RHO(I,J)-HFG*DPSIDH)	VOID0710
GO TO 200	VOID0720
C TWO-PHASE FLOW PARAMETERS WITHOUT BOILING.	VOID0730



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150 ALPHA(I) = 0.                                VOID0740
    RHO(I,J) = 1./V(I)                            VOID0750
    VP(I) = V(I)                                  VOID0760
    U(I) = F(I,J)/A(I)*VP(I)                     VOID0770
    UH(I) = U(I)                                  VOID0780
    PHI(I) = 1.                                    VOID0790
    QUAL(I) = 0.                                    VOID0800
200 CONTINUE                                       VOID0810
    RETURN                                          VOID0820
    END                                             VOID0830
*DECK,MIX
    SUPROUTINE MIX(J)                               MIX00010
C   THIS PROCEDURE CONTAINS THE COMMON AND TYPE STATEMENTS SHARED BY THEMIX00020
C   MAJOR SUBROUTINES OF CORRA-IIIC.              MIX00030
    COMMON KIJ, FTM, ABETA, BBETA, AFLUX, Z, THETA, PI, NAX, FLO, MIX00040
    1 GC, I3, I2, NCHANL, NK, IERROR, KDEBUG, NAXL, NGAPS, NGXL, MIX00050
    2 NAFAC, NODES, NSCBC, NBRC, J1, J2, J3, J4, J5, J6, J7, MIX00060
    3 ATOTAL, DX, DT, GK, NV, NF, AV(7), AF(7), QAX, FSPLIT(30) MIX00070
    4 , ELEV, NOX, SL, FERROF, ITERAT, NRAMP, NVISCW, NARAMP MIX00080
    COMMON PP(30), TT(30), VVF(30), VVG(30), HHF(30), HHG(30), MIX00090
    1 UUF(30), KKF(30), SSIGMA(30), NPROP, PREF, TF, VF, VG, HF, HG, MIX00100
    2 UF, KF, SIGMA, HFG, VFG, RHOF, RHOG MIX00110
    COMMON V(30), VP(30), VISC(30), VISCW(30), HFILM(30), CON(30), MIX00120
    1 CP(30), FSP(30), FMULT(30), U(30), UH(30), ALPHA(30), QUAL(30), MIX00130
    2 RHO(30,31), VPA(30), T(30), MINLET(30), FINLET(30) MIX00140
    COMMON COND(47), WP(47), GAP(47), FACTOR(47), IK(47), MIX00150
    1 JK(47), GAPN(47), LENGTH(47), USTAR(47), W(47,31) MIX00160
    COMMON A(30), AN(30), DHYD(30), DHYDN(30), DFDX(30), MIX00170
    1 DHDX(30), DPDX(30), QPRIM(30), PERIM(30), MIX00180
    2 HPERIM(30), NTYPE(30) MIX00190
    COMMON P(30,31), H(30,31), F(30,31), X(31) MIX00200
    COMMON WOLD(47,31), RHOOLD(30,31), FOLD(30,31), HOLD(30,31) MIX00210
    COMMON AXIAL(39), Y(39), IDAPEA(30), IDGAP(47), AA( 4), BB( 4), MIX00220
    1 CC( 4), AFACT(10,10), NCH(10), AXL(10), GAPXL(10), GFACT( 9,10), MIX00230
    2 NGAP( 9), BX(30), XQUAL(30) MIX00240
    COMMON NGRID, NGRIDT, GRIDXL(10), IGRID(10), CD(30, 5), MIX00250
    1 FXFLOW(47, 5), NGTYPE, GRID, FDIV(47) MIX00260
    LOGICAL FDIV, GRID MIX00270
    REAL KIJ, LENGTH, KF, KKF MIX00280
    NKK = NK MIX00290
    DO 240 K=1,NKK MIX00300
    COND(K) = 0. MIX00310
    II = IK(K) MIX00320
    JJ = JK(K) MIX00330
    DAVG = 4.*(A(II)+A(JJ))/(PERIM(II)+PERIM(JJ)) MIX00340
    GAVG = (F(II,J)+F(JJ,J))/(A(II)+A(JJ)) MIX00350
    XAVG = 0. MIX00360
    IF (AMAX1(QUAL(II),QUAL(JJ)) .GT. 0.) XAVG = .5*(QUAL(II)+QUAL(JJ)) MIX00370
    IF (XAVG.GT.0..AND.NBRC.GE.2) GO TO 80 MIX00380
    UAVG = 0.5*(VISC(II)+VISC(JJ)) MIX00390
    IF (NSCHC.EQ.1) RE = GAVG*DAVG/UAVG MIX00400
    IF (NSCHC.EQ.0) WP(K) = GAP(K)*GAVG*ABETA MIX00410
    IF (NSCHC.EQ.1) WP(K) = GAP(K)*GAVG*ABETA*RE**BBETA MIX00420
    IF (NSCHC.EQ.2) WP(K) = DAVG*GAVG*ABETA*RE**BBETA MIX00430
    IF (NSCHC.EQ.3 .AND. LENGTH(K).LE.0.) GO TO 1000 MIX00440
    IF (NSCHC.EQ.3) WP(K) = GAP(K)/LENGTH(K)*DAVG*GAVG*ABETA*RE**BBETA MIX00450
    WP(K) = WP(K)*FACTOR(K) MIX00460
    GO TO 100 MIX00470
80 CALL CURVE (XBETA,XAVG,BX,XQUAL,NBRC,IERROR,1) MIX00480

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IF (IEPROR.GT.1) GO TO 1000	MIX00490
WP(K) = GAVG*DAVG*XBETA*FACTOR(K)	MIX00500
100 IF (JS.FQ.0) GO TO 240	MIX00510
CAVG = 0.5*(CON(II)+CON(JJ))	MIX00520
IF (LENGTH(K).LE.0.) GO TO 1000	MIX00530
COND(K) = CAVG*GAP(K)/LENGTH(K)*GK*FACTOR(K)	MIX00540
240 CONTINUE	MIX00550
RETURN	MIX00560
1000 IEPROR = 4	MIX00570
RETURN	MIX00580
END	MIX00590
*DECK AREA	
SUBROUTINE AREA(J)	AREA0010
C THIS PROCEDURE CONTAINS THE COMMON AND TYPE STATEMENTS SHARED BY THE	AREA0020
C MAJOR SUBROUTINES OF COBRA-IIIC.	AREA0030
COMMON KIJ, FTM, ABETA, BBETA, AFLUX, Z, THETA, PI, NAX, FLO,	AREA0040
1 GC, I3, I2, NCHANL, NK, IERROR, KDEBUG, NAXL, NGAPS, NGXL,	AREA0050
2 NAFAC, NODS, NSCBC, NRRC, J1, J2, J3, J4, J5, J6, J7,	AREA0060
3 ATOTAL, DX, DT, GK, NV, NF, AV(7), AF(7), QAX, FSPLIT(30)	AREA0070
4 FLEV, NDX, SL, FERROR, ITERAT, NRAMP, NVISCW, NARAMP	AREA0080
COMMON PP(30), TT(30), VVF(30), VVG(30), HHF(30), HHG(30),	AREA0090
1 UUF(30), KKF(30), SSIGMA(30), NPROP, PREF, TF, VF, VG, HF, HG,	AREA0100
2 UF, KF, SIGMA, HFG, VFG, RHOF, RHOG	AREA0110
COMMON V(30), VP(30), VISC(30), VISCW(30), HFILM(30), CON(30),	AREA0120
1 CP(30), FSP(30), FMULT(30), U(30), UH(30), ALPHA(30), QUAL(30),	AREA0130
2 RHO(30,31), VPA(30), T(30), HINLET(30), FINLET(30)	AREA0140
COMMON COND(47), WP(47), GAP(47), FACTOR(47), IK(47),	AREA0150
1 JK(47), GAPN(47), LENGTH(47), USTAR(47), W(47,31)	AREA0160
COMMON A(30), AN(30), DHYD(30), DHYDN(30), DFDX(30),	AREA0170
1 DHDX(30), DPDX(30), OPRIM(30), PERIM(30),	AREA0180
2 HPERIM(30), NTYPE(30)	AREA0190
COMMON P(30,31), H(30,31), F(30,31), X(31)	AREA0200
COMMON WOLD(47,31), RHOOLD(30,31), FOLD(30,31), HOLD(30,31)	AREA0210
COMMON AXIAL(39), Y(39), IDAREA(30), IDGAP(47), AA( 4), BB( 4),	AREA0220
1 CC( 4), AFACT(10,10), NCH(10), AXL(10), GAPXL(10), GFACT( 9,10),	AREA0230
2 NGAP( 9), BX(30), XQUAL(30)	AREA0240
COMMON NGRID, NGRIDT, GRIDXL(10), IGRID(10), CD(30, 5),	AREA0250
1 FXFLOW(47, 5), NGTYPE, GRID, FDIV(47)	AREA0260
LOGICAL FDIV, GRID	AREA0270
REAL KIJ, LENGTH, KF, KKF	AREA0280
COMMON /RWRAP/ XCROSS(47,6), DUR(47), DIA, THICK, NWRAP(47), PITCH	AREA0290
DIMENSION AFAC(10), GFAC(10)	AREA0300
C	AREA0310
C CALCULATE CHANNEL AREA IF REQUIRED.	AREA0320
DO 5 I=1,NCHANL	AREA0330
A(I) = AN(I)	AREA0340
5 DHYD(I) = DHYDN(I)	AREA0350
IF (NAXL.EQ.0) GO TO 101	AREA0360
DO 100 I=1,NCHANL	AREA0370
JJ = IDAREA(I)	AREA0380
IF (JJ.LT.1) GO TO 100	AREA0390
DO 10 K=1,NAXL	AREA0400
10 AFAC(K) = AFACT(JJ,K)	AREA0410
CALL CURVE (FF,X(J)/Z,AFAC,AXL,NAXL,IERROR,1)	AREA0420
IF (IERROR.GT.1) GO TO 1000	AREA0430
IF (DT.LT.100.) GO TO 20	AREA0440
DUMY = FLOAT(ITERAT)/FLOAT(NARAMP)	AREA0441
IF (DUMY.GT.1.) DUMY = 1.	AREA0442
IF (FF.LE.0.) GO TO 1000	AREA0443

FF = 1.-(1.-FF)*DUMY	AREA0444
20 A(I) = AN(I)*FF	AREA0445
DHYD(I) = DHYDN(I)*FF	AREA0450
100 CONTINUE	AREA0460
101 IF(J6.NE.1) GO TO 110	AREA0470
C MODIFY APEA AND HYDRAULIC DIAMETER FOR WIRE WRAPS IN SUBCHANNELS.	AREA0480
DO 102 I=1,NCHANL	AREA0490
A(I) = A(I)-FLOAT(NWRAP(I))*PI*THICK**2*0.25	AREA0500
102 DHYD(I) = 4.*A(I)/(PERIM(I)*FLOAT(NWRAP(I))*PI*THICK)	AREA0510
C	AREA0520
C CALCULATE GAP SPACING IF REQUIRED.	AREA0530
110 IF(NGXL.EQ.0) GO TO 210	AREA0540
DO 200 K=1,NK	AREA0550
GAP(K) = GAPN(K)	AREA0560
L = IDGAP(K)	AREA0570
IF(L.LT.1) GO TO 200	AREA0580
DO 120 I=1,NGXL	AREA0590
120 GFAC(I) = GFAC(L,I)	AREA0600
CALL CURVE (FF,X(J)/Z,GFAC,GAPXL,NGXL,IEPROR,1)	AREA0610
IF(IEPROR.GT.1) GO TO 1000	AREA0620
IF(FF.LE.0.) GO TO 1000	AREA0625
GAP(K) = GAPN(K)*FF	AREA0630
200 CONTINUE	AREA0640
210 RETURN	AREA0650
1000 IEPROR = 9	AREA0660
RETURN	AREA0670
END	AREA0680
*DECK,FORCE	
SUBROUTINE FORCE(J)	FORC0010
C THIS PROCEDURE CONTAINS THE COMMON AND TYPE STATEMENTS SHARED BY THE	FORC0020
C MAJOR SUBROUTINES OF CORRA-IIIC.	FORC0030
COMMON KIJ, FTM, ABETA, BBETA, AFLUX, Z, THETA, PI, NAX, FLO,	FORC0040
1 GC, I3, I2, NCHANL, NK, IERROR, KDEBUG, NAXL, NGAPS, NGXL,	FORC0050
2 NAFAC, NODES, NSCBC, NARC, J1, J2, J3, J4, J5, J6, J7,	FORC0060
3 ATOTAL, DX, DT, GK, NV, NF, AV(7), AF(7), QAX, FSPLIT(30)	FORC0070
4 , ELEV, NDX, SL, FERROR, ITPAT, NPAMP, NVISCW, NARAMP	FORC0080
COMMON PP(30), TT(30), VVF(30), VVG(30), HHF(30), HHG(30),	FORC0090
1 UUF(30), KKF(30), SSIGMA(30), NPROR, PREF, TF, VF, VG, HF, HG,	FORC0100
2 UF, KF, SIGMA, HFG, VFG, RHOF, RHOG	FORC0110
COMMON V(30), VP(30), VISC(30), VISCW(30), HFILM(30), CON(30),	FORC0120
1 CP(30), FSP(30), FMULT(30), U(30), UH(30), ALPHA(30), QUAL(30),	FORC0130
2 RHO(30,31), VPA(30), T(30), HINLET(30), FINLET(30)	FORC0140
COMMON COND(47), WP(47), GAP(47), FACTOR(47), IK(47),	FORC0150
1 JK(47), GAPN(47), LENGTH(47), USTAR(47), W(47,31)	FORC0160
COMMON A(30), AN(30), DHYD(30), DHYDN(30), DFDX(30),	FORC0170
1 DHDX(30), DPOX(30), QPRIM(30), PERIM(30),	FORC0180
2 HPERIM(30), NTYPE(30)	FORC0190
COMMON P(30,31), H(30,31), F(30,31), X(31)	FORC0200
COMMON WOLD(47,31), RMOOLD(30,31), FOLD(30,31), HOLD(30,31)	FORC0210
COMMON AXIAL(39), Y(39), IQAREA(30), IDGAP(47), AA( 4), RB( 4),	FORC0220
1 CC( 4), AFACT(10,10), NCH(10), AXL(10), GAPXL(10), GFAC( 9,10),	FORC0230
2 NGAP( 9), BX(30), XQUAL(30)	FORC0240
COMMON NGRID, NGRIDT, GRIDXL(10), IGRID(10), CD(30, 5),	FORC0250
1 FXFLOW(47, 5), NGTYPE, GRID, FDIV(47)	FORC0260
LOGICAL FDIV, GRID	FORC0270
REAL KIJ, LENGTH, KF, KKF	FORC0280
COMMON /BWRAP/ XCROSS(47,6), DUR(47), DIA, THICK, NWRAP(47), PITCH	FORC0290
NKK = NK	FORC0300
DO 10 K=1,NKK	FORC0310

FDIV(K) = .FALSE.	FORC0320
10 CONTINUE	FORC0330
IF(J6.EQ.0) RETURN	FORC0340
JM1 = J-1	FORC0350
GO TO (100,200),J6	FORC0360
C FORCED DIVERSION CROSSFLOW FROM WIRE WRAPS	FORC0370
100 IF(PITCH.LE.0.) GO TO 1000	FORC0380
NN = Z/PITCH	FORC0390
NN = NN+1	FORC0400
DO 115 K=1,NN	FORC0410
IF(X(J).LE.PITCH*FLOAT(K)) GO TO 118	FORC0420
115 CONTINUE	FORC0430
118 PL = K-1	FORC0440
C PL IS THE PITCH LENGTH CONTAINING X(J).	FORC0450
C FIND THE WRAP CROSSINGS IN DX.	FORC0460
DO 130 K=1,NK	FORC0470
II = IK(K)	FORC0480
JJ = JK(K)	FORC0490
DO 130 L=1,6	FORC0500
IF(XCROSS(K,L)) 119,130,119.	FORC0510
119 XC = (ABS(XCROSS(K,L))+PL)*PITCH	FORC0520
IF(XC.GT.X(J) .OR. XC.LE.X(JM1)) GO TO 130	FORC0530
FDIV(K) = .TRUE.	FORC0540
C ADD AND SUBTRACT WIRE WRAPS FROM SUBCHANNEL AT EACH WRAP CROSSING.	FORC0550
IF(XCROSS(K,L)) 120,130,121	FORC0560
120 NWRAP(II) = NWRAP(II)+1	FORC0570
NWRAP(JJ) = NWRAP(JJ)-1	FORC0580
GO TO 123	FORC0590
121 NWRAP(II) = NWRAP(II)-1	FORC0600
NWRAP(JJ) = NWRAP(JJ)+1	FORC0610
IF(NRAMP.LE.0) GO TO 1000	FORC0620
123 DUMY = FLOAT(ITERAT)/FLOAT(NRAMP)	FORC0630
IF(DUMY.GT.1.) DUMY = 1.	FORC0640
W(K,J) = GAP(K)*PI*(DIA+THICK)*DUR(K)/DX*DUMY	FORC0650
IF(XCROSS(K,L)) 124,130,125	FORC0660
124 W(K,J) = -W(K,J)*F(JJ,J)/A(JJ)	FORC0670
W(K,J) = W(K,J)*FACTOR(K)	FORC0675
GO TO 130	FORC0680
125 W(K,J) = W(K,J)*F(II,J)/A(II)	FORC0690
W(K,J) = W(K,J)*FACTOR(K)	FORC0695
130 CONTINUE	FORC0700
RETURN	FORC0710
200 IF(.NOT.GRID) RETURN	FORC0720
DO 230 K=1,NKK	FORC0730
IF(ABS(FXFLOW(K,NGTYPE)).LT.1.E-10) GO TO 230	FORC0740
C ZERO FORCED FLOW FRACTION DOES NOT BLOCK THE NATURAL DIVERSION CROSSFLOW	FORC0750
II = IK(K)	FORC0760
JJ = JK(K)	FORC0770
FDIV(K) = .TRUE.	FORC0780
IF(NRAMP.LE.0) GO TO 1000	FORC0790
DUMY = FLOAT(ITERAT)/FLOAT(NRAMP)	FORC0800
IF(DUMY.GT.1.) DUMY = 1.	FORC0810
DUMY = DUMY*FXFLOW(K,NGTYPE)/DX	FORC0820
IF(DUMY.GT.0.) W(K,J) = DUMY*F(II,J)	FORC0830
IF(DUMY.LT.0.) W(K,J) = DUMY*F(JJ,J)	FORC0840
W(K,J) = W(K,J)*FACTOR(K)	FORC0845
230 CONTINUE	FORC0850
RETURN	FORC0860
1000 IERROR = 6	FORC0870

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RETURN
END
*DECK,CIJ
FUNCTION CIJ(K,J)
C THIS PROCEDURE CONTAINS THE COMMON AND TYPE STATEMENTS SHARED BY THE
C MAJOR SUBROUTINES OF CORRA-IIIC.
COMMON KIJ, FTM, ABETA, BBETA, AFLUX, Z, THETA, PI, NAX, FLO,
1 GC, I3, I2, NCHANL, NK, IERROR, KDEBUG, NAXL, NGAPS, NGXL,
2 NAFAC, NODES, NSCBC, NBRC, J1, J2, J3, J4, J5, J6, J7,
3 ATOTAL, DX, DT, GK, NV, NF, AV(7), AF(7), QAX, FSPLIT(30)
4 , ELEV, NDX, SL, FERROR, ITERAT, NRAMP, NVISCW, NARAMP
COMMON PP(30), TT(30), VVF(30), VVG(30), HHF(30), HHG(30),
1 UUF(30), KKF(30), SSIGMA(30), NPROP, PREF, TF, VF, VG, HF, HG,
2 UF, KF, SIGMA, HFG, VFG, RHOF, RHOG
COMMON V(30), VP(30), VISC(30), VISCW(30), HFILM(30), CON(30),
1 CP(30), FSP(30), FMULT(30), U(30), UH(30), ALPHA(30), QUAL(30),
2 RHO(30,31), VPA(30), T(30), HINLET(30), FINLET(30)
COMMON COND(47), WP(47), GAP(47), FACTOR(47), IK(47),
1 JK(47), GAPN(47), LENGTH(47), USTAR(47), W(47,31)
COMMON A(30), AN(30), DHYD(30), DHYDN(30), DFDX(30),
1 DHDX(30), DPDX(30), OPRIM(30), PERIM(30),
2 MPERIM(30), NTYPE(30)
COMMON P(30,31), H(30,31), F(30,31), X(31)
COMMON WOLD(47,31), RHOOLD(30,31), FOLD(30,31), HOLD(30,31)
COMMON AXIAL(39), Y(39), IDAREA(30), IDGAP(47), AA( 4), BB( 4),
1 CC( 4), AFACT(10,10), NCH(10), AXL(10), GAPXL(10), GFACT( 9,10),
2 NGAP( 9), BX(30), XQUAL(30)
COMMON NGRID, NGRIDT, GRIDXL(10), IGRID(10), CD(30, 5),
1 FAFLOW(47, 5), NGTYPE, GRID, FDIV(47)
LOGICAL FDIV, GRID
REAL KIJ, LENGTH, KF, KKF
IF(GAP(K).LE.0.) GO TO 1000
II = IK(K)
JJ = JK(K)
RSTAR = RHO(II,J)
IF(W(K,J).LT.0.) RSTAR = RHO(JJ,J)
WMIN = ABS(W(K,J))
IF(WMIN.LT..001) WMIN = .001
CIJ = KIJ*WMIN/2./GC/RSTAR/GAP(K)/GAP(K)
CIJ = CIJ/FACTOR(K)**2
RETURN
1000 IERROR = 18
RETURN
END
*DECK,SPLIT
SUBROUTINE SPLIT
C THIS PROCEDURE CONTAINS THE COMMON AND TYPE STATEMENTS SHARED BY THE
C MAJOR SUBROUTINES OF CORRA-IIIC.
COMMON KIJ, FTM, ABETA, BBETA, AFLUX, Z, THETA, PI, NAX, FLO,
1 GC, I3, I2, NCHANL, NK, IERROR, KDEBUG, NAXL, NGAPS, NGXL,
2 NAFAC, NODES, NSCBC, NBRC, J1, J2, J3, J4, J5, J6, J7,
3 ATOTAL, DX, DT, GK, NV, NF, AV(7), AF(7), QAX, FSPLIT(30)
4 , ELEV, NDX, SL, FERROR, ITERAT, NRAMP, NVISCW, NARAMP
COMMON PP(30), TT(30), VVF(30), VVG(30), HHF(30), HHG(30),
1 UUF(30), KKF(30), SSIGMA(30), NPROP, PREF, TF, VF, VG, HF, HG,
2 UF, KF, SIGMA, HFG, VFG, RHOF, RHOG
COMMON V(30), VP(30), VISC(30), VISCW(30), HFILM(30), CON(30),
1 CP(30), FSP(30), FMULT(30), U(30), UH(30), ALPHA(30), QUAL(30),
2 RHO(30,31), VPA(30), T(30), HINLET(30), FINLET(30)
SPLT0010
SPLT0020
SPLT0030
SPLT0040
SPLT0050
SPLT0060
SPLT0070
SPLT0080
SPLT0090
SPLT0100
SPLT0110
SPLT0120
SPLT0130
SPLT0140

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COMMON COND(47), WP(47), GAP(47), FACTOR(47), IK(47),
1 JK(47), GAPN(47), LENGTH(47), USTAR(47), W(47,31)
COMMON A(30), AN(30), QHYD(30), QHYDN(30), DFOX(30),
1 DHOX(30), DPDX(30), QPRIM(30), PERIM(30),
2 HPERIM(30), NTYPE(30)
COMMON P(30,31), H(30,31), F(30,31), X(31)
COMMON WOLD(47,31), RHOOLD(30,31), FOLD(30,31), HOLD(30,31)
COMMON AXIAL(39), Y(39), IDAREA(30), IDGAP(47), AA( 4), BB( 4),
1 CC( 4), AFACT(10,10), NCH(10), AXL(10), GAPXL(10), GFACT( 9,10),
2 NGAP( 9), HX(30), XQUAL(30)
COMMON NGRID, NGRIDT, GRIDXL(10), IGRID(10), CD(30, 5),
1 FXFLOW(47, 5), NGTYPE, GRID, FDIV(47)
LOGICAL FDIV, GRID
REAL KIJ, LENGTH, KF, KKF
COMMON /DP/ DPK(30)
NCHAN = NCHANL
C CORRECT FLOW ESTIMATE BY ITERATION. THIS PROCEDURE ASSUMES THERE IS NSPLT0150
C DENSITY CHANGE WITH LENGTH AND THAT NO DIVERSION CROSSFLOW IS OCCURRISPLT0160
C CONVERGENCE TOLERANCE IS E. SPLT0170
E=0.005 SPLT0180
SAVEDT = DT SPLT0190
DT = 1.E+10 SPLT0200
DO 10 I=1,NCHANL SPLT0210
F(I,1) = FINLET(I) SPLT0220
10 H(I,1) = HINLET(I) SPLT0230
DO 100 K=1,200 SPLT0240
CALL PROP(2,1) SPLT0250
IF(IEPROR.GT.1) GO TO 1000 SPLT0260
CALL VOID(I) SPLT0270
DO 15 I=1,NCHANL SPLT0280
15 VPA(I) = VP(I)/A(I) SPLT0290
IF(IEPROR.GT.1) GO TO 1000 SPLT0300
IF(FTM.GT.0.) CALL MIX(I) SPLT0310
IF(IEPROR.GT.1) GO TO 1000 SPLT0320
CALL DIFFER(3,1) SPLT0330
IF(IEPROR.GT.1) GO TO 1000 SPLT0340
DPAVG = 0. SPLT0350
DO 20 I=1,NCHANL SPLT0360
20 DPAVG = DPAVG + DPDX(I)*A(I) SPLT0370
DPAVG = DPAVG/ATOTAL SPLT0380
J=2 SPLT0390
FTOT = 0. SPLT0400
DO 30 I=1,NCHANL SPLT0410
DELTA F = (DPAVG-DPDX(I))/2./DPDX(I)*F(I,1) SPLT0420
IF(FTM.GT.0.) DELTA F = DELTA F*0.5 SPLT0430
FSAVE = F(I,1) SPLT0440
F(I,1) = F(I,1) + DELTA F SPLT0450
IF(F(I,1).LT.0.) GO TO 1000 SPLT0460
IF(ABS(F(I,1)-FSAVE)/FSAVE .GT. E) J=1 SPLT0470
FTOT = FTOT + F(I,1) SPLT0480
30 CONTINUE SPLT0490
DO 40 I=1,NCHANL SPLT0500
F(I,1) = F(I,1)*FLO/FTOT SPLT0510
40 FINLET(I) = F(I,1) SPLT0520
IF(J.GT.1) GO TO 120 SPLT0530
100 CONTINUE SPLT0540
1000 WRITE(13,1) (I,F(I,1),DPDX(I),I=1,NCHAN) SPLT0550
1 FORMAT(40H FLOW SPLIT TO GIVE EQUAL DP/DX FAILED /((15,2E14,6)) SPLT0560
IFERROR = 8 SPLT0570
SPLT0580
SPLT0590
SPLT0600
SPLT0610
SPLT0620
SPLT0630
SPLT0640
SPLT0650
SPLT0660
SPLT0670
SPLT0680
SPLT0690
SPLT0700
SPLT0710
SPLT0720
SPLT0730

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120 DT = SAVEDT                                SPLT0740
RETURN                                           SPLT0750
END                                              SPLT0760
*DECK,S
FUNCTION S(K,I)                                S0000010
C THIS PROCEDURE CONTAINS THE COMMON AND TYPE STATEMENTS SHARED BY THE S0000020
C MAJOR SUBROUTINES OF COBRA-IIIC.            S0000030
COMMON KIJ, FTM, ABETA, BBETA, AFLUX, Z, THETA, PI, NAX, FLO, S0000040
1 GC, I3, I2, NCHANL, NK, IERROR, KDEBUG, NAXL, NGAPS, NGXL, S0000050
2 NAFACT, NODES, NSCBC, NBRC, J1, J2, J3, J4, J5, J6, J7, S0000060
3 ATOTAL, DX, DT, GK, NV, NF, AV(7), AF(7), QAX, FSPLIT(30) S0000070
4 ELEV, NDX, SL, FERROR, ITERAT, NRAMP, NVISCW, NARAMP S0000080
COMMON PP(30), TT(30), VVF(30), VVG(30), HHF(30), HHG(30), S0000090
1 UUF(30), KKF(30), SSIGMA(30), NPROP, PREF, TF, VF, VG, HF, HG, S0000100
2 UF, KF, SIGMA, HFG, VFG, RHOF, RHOG S0000110
COMMON V(30), VP(30), VISC(30), VISCW(30), HFILM(30), CON(30), S0000120
1 CP(30), FSP(30), FMULT(30), U(30), UH(30), ALPHA(30), QUAL(30), S0000130
2 RHO(30,31), VPA(30), T(30), HINLET(30), FINLET(30) S0000140
COMMON COND(47), WP(47), GAP(47), FACTOR(47), IK(47), S0000150
1 JK(47), GAPN(47), LENGTH(47), USTAR(47), W(47,31) S0000160
COMMON A(30), AN(30), DHYD(30), DHYDN(30), DFDX(30), S0000170
1 DHDX(30), DPOX(30), QPRIM(30), PERIM(30), S0000180
2 HPERIM(30), NTYPE(30) S0000190
COMMON P(30,31), H(30,31), F(30,31), X(31) S0000200
COMMON WOLD(47,31), RHOOLD(30,31), FOLD(30,31), HOLD(30,31) S0000210
COMMON AXIAL(39), Y(39), IDAREA(30), IDGAP(47), AA( 4), BB( 4), S0000220
1 CC( 4), AFACT(10,10), NCH(10), AXL(10), GAPXL(10), GFACT( 9,10), S0000230
2 NGAP( 9), RX(30), XQUAL(30) S0000240
COMMON NGRID, NGRIDT, GRIDT, GRIDXL(10), IGRID(10), CD(30, 5), S0000250
1 FXFLOW(47, 5), NGTYPE, GRID, FDIV(47) S0000260
LOGICAL FDIV, GRID S0000270
REAL KIJ, LENGTH, KF, KKF S0000280
S = 0. S0000290
IF(I.EQ.IK(K)) S = 1. S0000300
IF(I.EQ.JK(K)) S = -1. S0000310
RETURN S0000320
END S0000330
*DECK,SCQUAL
FUNCTION SCQUAL(I,J)                          SCQL0010
C LEVY SUBCOOLED MODEL. CALCULATES TRUE QUALITY AS A CORRECTION TO SCQL0020
C THE EQUILIBRIUM QUALITY.                   SCQL0030
COMMON KIJ, FTM, ABETA, BBETA, AFLUX, Z, THETA, PI, NAX, FLO, SCQL0040
1 GC, I3, I2, NCHANL, NK, IERROR, KDEBUG, NAXL, NGAPS, NGXL, SCQL0050
2 NAFACT, NODES, NSCBC, NBRC, J1, J2, J3, J4, J5, J6, J7, SCQL0060
3 ATOTAL, DX, DT, GK, NV, NF, AV(7), AF(7), QAX, FSPLIT(30) SCQL0070
4 ELEV, NDX, SL, FERROR, ITERAT, NRAMP, NVISCW, NARAMP SCQL0080
COMMON PP(30), TT(30), VVF(30), VVG(30), HHF(30), HHG(30), SCQL0090
1 UUF(30), KKF(30), SSIGMA(30), NPROP, PREF, TF, VF, VG, HF, HG, SCQL0100
2 UF, KF, SIGMA, HFG, VFG, RHOF, RHOG SCQL0110
COMMON V(30), VP(30), VISC(30), VISCW(30), HFILM(30), CON(30), SCQL0120
1 CP(30), FSP(30), FMULT(30), U(30), UH(30), ALPHA(30), QUAL(30), SCQL0130
2 RHO(30,31), VPA(30), T(30), HINLET(30), FINLET(30) SCQL0140
COMMON COND(47), WP(47), GAP(47), FACTOR(47), IK(47), SCQL0150
1 JK(47), GAPN(47), LENGTH(47), USTAR(47), W(47,31) SCQL0160
COMMON A(30), AN(30), DHYD(30), DHYDN(30), DFDX(30), SCQL0170
1 DHDX(30), DPOX(30), QPRIM(30), PERIM(30), SCQL0180
2 HPERIM(30), NTYPE(30) SCQL0190
COMMON P(30,31), H(30,31), F(30,31), X(31) SCQL0200
COMMON WOLD(47,31), RHOOLD(30,31), FOLD(30,31), HOLD(30,31) SCQL0210

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COMMON AXIAL(39), Y(39), IDAREA(30), IDGAP(47), AA( 4), RB( 4), SCQL0220
1 CC( 4), AFACT(10,10), NCH(10), AXL(10), GAPXL(10), GFACT( 9,10), SCQL0230
2 NGAP( 9), RX(30), XQUAL(30) SCQL0240
COMMON NGRID, NGRIDT, GRIDXL(10), IGRID(10), CD(30, 5), SCQL0250
1 FXFLOW(47, 5), NGTYPE, GRID, FDIV(47) SCQL0260
LOGICAL FDIV, GRID SCQL0270
REAL KIJ, LENGTH, KF, KKF SCQL0280
XP = QUAL(I) SCQL0290
SCQUAL = XP SCQL0300
IF(OPRIM(I).LE.0.) RETURN SCQL0310
CNC = 0.015 SCQL0320
YB = CNC/VISC(I)*SORT(SIGMA*GC*DHYD(I)/V(I)) SCQL0330
TAUW = FSP(I)*.125*V(I)*(F(I,J)/A(I))**2/GC SCQL0340
PR = CP(I)*VISC(I)/CON(I) SCQL0350
Q = OPRIM(I)/(4PERIM(I)/V(I)*CP(I)*SORT(TAUW*GC*V(I))) SCQL0360
DELTAT = QPRIM(I)/4PERIM(I)/HFILM(I) SCQL0370
IF(YB.GE.5..AND. YB.LT.30.)DELTAT = DELTAT - 5.*Q*(PR+ALOG(1.+PR*( SCQL0390
1 YB*.2-1.))) SCQL0400
IF(YB.GE.30.) DELTAT = DELTAT - 5.*Q*(PR+ALOG(1.+5.*PR) SCQL0410
1 + .5*ALOG(YB/30.)) SCQL0420
XD = -CP(I)*DELTAT/HFG SCQL0430
IF(QUAL(I).LT.XD) GO TO 140 SCQL0440
ARG = QUAL(I)/XD - 1. SCQL0450
IF(ARG.GT.0.) ARG = 0. SCQL0460
XP = QUAL(I) - XD*EXP(ARG) SCQL0470
140 SCQUAL = XP SCQL0480
RETURN SCQL0490
END SCQL0500
*DECK,BVOID
FUNCTION BVOID(I,J) BVOD0010
C BVOID CALCULATES THE BULK VOID FRACTION GIVEN A QUALITY. BVOD0020
COMMON KIJ, FTM, ABETA, RBETA, AFLUX, Z, THETA, PI, NAX, FLO, BVOD0030
1 GC, I3, I2, NCHANL, NK, IERROR, KDEBUG, NAXL, NGAPS, NGXL, BVOD0040
2 NAFAC, NODES, NSCBC, NARC, J1, J2, J3, J4, J5, J6, J7, BVOD0050
3 ATOTAL, DX, DT, GK, NV, NF, AV(7), AF(7), QAX, FSPLIT(30) BVOD0060
4 , ELEV, NDX, SL, FERPOR, ITERAT, NPAMP, NVISCW, NARAMP BVOD0070
COMMON PP(30), TT(30), VVF(30), VVG(30), HHF(30), HHG(30), BVOD0080
1 UJIF(30), KKF(30), SSIGMA(30), NPROP, PREF, TF, VF, VG, HF, HG, BVOD0090
2 UF, KF, SIGMA, HFG, VFG, RHOF, RHOG BVOD0100
COMMON V(30), VP(30), VISC(30), VISCW(30), HFILM(30), CON(30), BVOD0110
1 CP(30), FSP(30), FMULT(30), U(30), UH(30), ALPHA(30), QUAL(30), BVOD0120
2 PHO(30,31), VPA(30), T(30), HINLET(30), FINLET(30) BVOD0130
COMMON COND(47), WP(47), GAP(47), FACTOR(47), IK(47), BVOD0140
1 JK(47), GAPN(47), LENGTH(47), USTAR(47), W(47,31) BVOD0150
COMMON A(30), AN(30), DHYD(30), DHYDN(30), DFDX(30), BVOD0160
1 DHDX(30), DPDX(30), OPRIM(30), PERIM(30), BVOD0170
2 4PERIM(30), NTYPE(30) BVOD0180
COMMON P(30,31), H(30,31), F(30,31), X(31) BVOD0190
COMMON WOLD(47,31), PHOOLD(30,31), FOLD(30,31), HOLD(30,31) BVOD0200
COMMON AXIAL(39), Y(39), IDAREA(30), IDGAP(47), AA( 4), RB( 4), BVOD0210
1 CC( 4), AFACT(10,10), NCH(10), AXL(10), GAPXL(10), GFACT( 9,10), BVOD0220
2 NGAP( 9), RX(30), XQUAL(30) BVOD0230
COMMON NGRID, NGRIDT, GRIDXL(10), IGRID(10), CD(30, 5), BVOD0240
1 FXFLOW(47, 5), NGTYPE, GRID, FDIV(47) BVOD0250
LOGICAL FDIV, GRID BVOD0260
REAL KIJ, LENGTH, KF, KKF BVOD0270
XP = QUAL(I) BVOD0280
BVOID = 0. BVOD0290
IF(XP.LE.0.) RETURN BVOD0300

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ALPHA(I) = 0.	HVOD0310
IF (J3.EQ.0) ALPHA(I) = XP*VG/((1.-XP)*VF+XP*VG)	HVOD0320
IF (J3.EQ.1) ALPHA(I) = (0.833+0.167*XP)*XP*VG/((1.-XP)*VF+XP*VG)	HVOD0330
IF (J3.EQ.5) ALPHA(I) = XP*VG/((1.-XP)*VF+AV(1)+XP*VG)	HVOD0340
IF (J3.NE.6) GO TO 90	HVOD0350
ALPHA(I) = AV(1)	HVOD0360
XX = QUAL(I)	HVOD0370
DO 80 K=2,NV	HVOD0380
ALPHA(I) = ALPHA(I)+AV(K)*XX	HVOD0390
90 XX = XX*QUAL(I)	HVOD0400
90 BVOID = ALPHA(I)	HVOD0410
RETURN	HVOD0420
END	HVOD0430
*DECK,DECOMP	
SUBROUTINE DECOMP (NN,IEROR)	DCOM0010
C SIMULTANEOUS LINEAR EQUATION SOLVER. REF - G. FORSYTHE AND C.B. MOLER	DCOM0020
C COMPUTER SOLUTION OF LINEAR ALGEBRAIC SYSTEMS. PRENTICE-HALL(1967).	DCOM0030
COMMON /BUL/ UL(47,47), X(47), B(47), IPS(47)	DCOM0040
DIMENSION SCALES(47)	DCOM0050
N = NN	DCOM0060
C	DCOM0070
C INITIALIZE IPS, UL AND SCALES	DCOM0080
NOUT = 6	DCOM0090
N = N	DCOM0100
DO 5 I = 1,N	DCOM0110
IPS(I) = I	DCOM0120
ROWNRM = 0.0	DCOM0130
N = N	DCOM0140
DO 2 J = 1,N	DCOM0150
IF (ROWNRM-ABS(UL(I,J))) 1,2,2	DCOM0160
1      ROWNRM = ABS(UL(I,J))	DCOM0170
2      CONTINUE	DCOM0180
IF (ROWNRM) 3,4,3	DCOM0190
3      SCALES(I) = 1.0/ROWNRM	DCOM0200
GO TO 5	DCOM0210
4      WRITE (NOUT,111)	DCOM0220
111 FORMAT(54HOMATRIX WITH ZERO ROW IN DECOMPOSE.	DCOM0230
IEROR = 12	DCOM0240
GO TO 100	DCOM0250
5      CONTINUE	DCOM0260
C	DCOM0270
C GAUSSIAN ELIMINATION WITH PARTIAL PIVOTING	DCOM0280
NM1 = N-1	DCOM0290
DO 17 K = 1,NM1	DCOM0300
BIG = 0.0	DCOM0310
DO 11 I = K,N	DCOM0320
IP = IPS(I)	DCOM0330
SIZE = ABS(UL(IP,K))*SCALES(IP)	DCOM0340
IF (SIZE-BIG) 11,11,10	DCOM0350
10      BIG = SIZE	DCOM0360
IDXPIV = I	DCOM0370
11      CONTINUE	DCOM0380
IF (BIG) 13,18,13	DCOM0390
13      IF (IDXPIV-K) 14,15,14	DCOM0400
14      J = IPS(K)	DCOM0410
IPS(K) = IPS(IDXPIV)	DCOM0420
IPS(IDXPIV) = J	DCOM0430
15      KP = IPS(K)	DCOM0440
PIVOT = UL(KP,K)	DCOM0450

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      KP1 = K+1
      DO 16 I = KP1,N
        IP = IPS(I)
        EM = -UL(IP,K)/PIVOT
        UL(IP,K) = -FM
        IF (EM) 20,16,20
C     INNER LOOP. CHECK EFFICIENCY OF COMPILED CODE.
C     IT MAY BE NECESSARY TO USE DOUBLE PRECISION WHEN COMPUTING THIS
C     LOOP TO PREVENT ROUNDOFF ERRORS DUE TO POORLY CONDITIONED MATRICES.
      20      DO 21 J = KP1,N
      21      UL(IP,J) = UL(IP,J) + EM*UL(KP,J)
      16      CONTINUE
      17      CONTINUE
      KP = IPS(N)
      IF (UL(KP,N)) 19,18,19
      18      PRINT 112
      100     PRINT 113, ((UL(K,L),L=1,NN),K=1,NN)
      113     FORMAT(7E14.8)
      112     FORMAT(54HOSINGULAR MATRIX IN DECOMPOSE. ZERO DIVIDE IN SOLVE.
      IERROR = 12
      19      RETURN
      END
*DECK.SOLVE
      SUBROUTINE SOLVE(NN)
      COMMON /HUL/ UL(47,47), X(47), R(47), IPS(47)
      N = NN
      NP1 = N+1
C
      IP = IPS(1)
      X(1) = B(IP)
      DO 2 I = 2,N
        IP = IPS(I)
        IM1 = I-1
        SUM = 0.0
C     DOUBLE PRECISION MAY BE REQUIRED FOR INNER LOOP.
      DO 1 J = 1,IM1
      1      SUM = SUM + UL(IP,J)*X(J)
      2      X(I) = B(IP) - SUM
C
      IP = IPS(N)
      X(N) = X(N)/UL(IP,N)
      DO 4 IBACK = 2,N
      I = NP1-IBACK
C     I GOES (N-1),.....1
      IP = IPS(I)
      IP1 = I+1
      SUM = 0.0
C     DOUBLE PRECISION MAY BE REQUIRED FOR INNER LOOP.
      DO 3 J = IP1,N
      3      SUM = SUM + UL(IP,J)*X(J)
      4      X(I) = (X(I)-SUM)/UL(IP,I)
      RETURN
      END
*DECK.CURVE
      SUBROUTINE CURVE (FX,X,F,Y,N,J,ISAVE)
      DIMENSION F(47), Y(47)
C     FX - QUANTITY TO BE FOUND
C     X - INDEPENDENT VARIABLE

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DCOM0460
DCOM0470
DCOM0480
DCOM0490
DCOM0500
DCOM0510
DCOM0520
DCOM0530
DCOM0540
DCOM0550
DCOM0560
DCOM0570
DCOM0580
DCOM0590
DCOM0600
DCOM0610
DCOM0620
DCOM0630
DCOM0640
DCOM0650
DCOM0660
DCOM0670
SOLV0010
SOLV0020
SOLV0030
SOLV0040
SOLV0050
SOLV0060
SOLV0070
SOLV0080
SOLV0090
SOLV0100
SOLV0110
SOLV0120
SOLV0130
SOLV0140
SOLV0150
SOLV0160
SOLV0170
SOLV0180
SOLV0190
SOLV0200
SOLV0210
SOLV0220
SOLV0230
SOLV0240
SOLV0250
SOLV0260
SOLV0270
SOLV0280
SOLV0290
SOLV0300
CURV0010
CURV0020
CURV0030
CURV0040
CURV0050

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C	F - INPUT ARRAY FOR THE ORDINATE (MONOTONIC WITH Y)	CURV0060
C	Y - INPUT ARRAY FOR THE ARCISSE (MONOTONIC INCREASE)	CURV0070
C	N - NUMBER OF F(I) OR Y(I) VALUES	CURV0080
C	J - ERROR SIGNAL. J=10	CURV0090
C		CURV0100
	1 FORMAT(49H TABULAK LOOKUP FAILED IN SUBROUTINE CURVE, FX = E12.6,	CURV0110
	1 6H X = F12.6 / (10E12.4))	CURV0120
	IF (ISAVE.LT.1 .OR. ISAVE.GT.2) GO TO 70	CURV0130
	GO TO (10,50),ISAVE	CURV0140
10	DO 20 I=1,N	CURV0150
	IF (X-Y(I)) 30,15,20	CURV0160
15	IF (I.EQ.N) GO TO 40	CURV0170
20	CONTINUE	CURV0180
	GO TO 60	CURV0190
30	IF (I.EQ.1) GO TO 60	CURV0200
40	B = (X-Y(I-1))/(Y(I)-Y(I-1))	CURV0210
50	FX = F(I-1) + 9*(F(I)-F(I-1))	CURV0220
	RETURN	CURV0230
60	PRINT 1, FX,X,(F(I),Y(I),I=1,N)	CURV0240
70	J = 10	CURV0250
	RETURN	CURV0260
	END	CURV0270
*DECK	TOD	
	SUBROUTINE TOD(A)	TOD00010
	DIMENSION TIME(2), A(2)	TOD00020
	DATA TIME / 6H . 6H /	TOD00030
	A(1) = TIME(1)	TOD00040
	A(2) = TIME(2)	TOD00050
	RETURN	TOD00060
	END	TOD00070
*DECK	DOY	
	SUBROUTINE DOY(A)	DOY00010
	DIMENSION DATE(2), A(2)	DOY00020
	DATA DATE / 6H . 6H /	DOY00030
	A(1) = DATE(1)	DOY00040
	A(2) = DATE(2)	DOY00050
	RETURN	DOY00060
	END	DOY00070
*DECK	ELAP	
	SUBROUTINE ELAP(MTIME)	ELAP0010
	MTIME = 0	ELAP0020
	RETURN	ELAP0030
	END	ELAP0040

SAMPLE INPUT CORRA III C  
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2000		CY-RUN III 7-(89). UPPER QUADRANT					RUN 026		
1	30								
640.493.3	0.02028	0.7203	479.8	1203.3	0.260	0.3521	0.00122		
640.500.0	0.02043	0.6761	487.7	1202.5	0.256	0.3494	0.00117		
720.506.4	0.02058	0.6366	495.3	1201.5	0.253	0.3463	0.00113		
760.512.5	0.02073	0.6011	502.6	1200.4	0.250	0.3434	0.00108		
800.518.4	0.02087	0.5691	509.7	1199.3	0.247	0.3405	0.00102		
840.524.0	0.02101	0.5400	516.6	1198.0	0.244	0.3377	0.00098		
880.529.5	0.02116	0.5134	523.3	1196.7	0.240	0.3350	0.00096		
920.534.7	0.02130	0.4890	529.8	1195.4	0.238	0.3325	0.00094		
960.539.9	0.02145	0.4666	536.2	1193.9	0.235	0.3299	0.00087		
1000.544.8	0.02159	0.4459	542.4	1192.4	0.233	0.3273	0.00083		
1050.550.7	0.02177	0.4222	550.0	1190.4	0.230	0.3242	0.00080		
1100.556.5	0.02195	0.4005	557.4	1188.3	0.227	0.3209	0.00075		
1150.562.0	0.02214	0.3806	564.6	1186.2	0.224	0.3177	0.00071		
1200.567.4	0.02232	0.3623	571.7	1183.9	0.222	0.3145	0.00068		
1250.572.6	0.02250	0.3454	578.6	1181.6	0.220	0.3113	0.00064		
1300.577.6	0.02269	0.3297	585.4	1179.2	0.218	0.3080	0.00061		
1350.582.5	0.02288	0.3152	592.1	1176.7	0.216	0.3047	0.00058		
1400.587.3	0.02307	0.3016	598.6	1174.1	0.215	0.3015	0.00056		
1450.591.9	0.02326	0.2888	605.1	1171.4	0.213	0.2982	0.00054		
1500.596.4	0.02346	0.2769	611.5	1168.7	0.211	0.2947	0.00052		
1550.600.8	0.02366	0.2657	617.8	1165.9	0.210	0.2913	0.00050		
1600.605.1	0.02386	0.2552	624.0	1162.9	0.207	0.2878	0.00048		
1650.609.2	0.02407	0.2452	630.2	1159.9	0.205	0.2845	0.00045		
1700.613.3	0.02428	0.2358	636.2	1156.9	0.203	0.2811	0.00043		
1750.617.3	0.02450	0.2268	642.3	1153.7	0.201	0.2776	0.00041		
1800.621.2	0.02494	0.2102	654.2	1147.0	0.200	0.2742	0.00040		
1900.628.8	0.02517	0.2025	660.1	1143.5	0.197	0.2673	0.00037		
1950.632.4	0.02541	0.1952	666.0	1140.0	0.194	0.2639	0.00035		
2000.636.0	0.02565	0.1881	671.9	1136.3	0.192	0.2604	0.00033		
2050.639.5	0.02590	0.1814	677.7	1132.5	0.190	0.2570	0.00031		

2 1 0 0 1  
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 3 39  
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 .11491.042.14471.024.17261.149.20041.192.22831.218.25621.233  
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 .45121.270.47911.157.50691.268.53481.270.56261.266.59051.254  
 .61831.229.64621.123.67411.190.70191.182.72981.152.75761.105  
 .78551.071.8133.9000.8412.8620.8691.7280.8969.5480.9248.3710  
 .9524.1750.95270.0001.0000.000

4	30	30				
1	1.17711.3261.326	2 .141	3 .141	12 .282		
1	2.15421.421.9943	4 .141	12.0805			
1	3.15421.421.9943	4.0805	12.2215			
1	4.15421.421.9943	12.2215				
1	538.37322.8270.5	62.136	92.136			
1	619.12157.2135.2	101.068				
1	738.37322.8270.5	82.136	122.136			
1	838.37314.4270.5	92.136	132.136			
1	938.37305.9270.5	102.136	142.136			
1	1019.18153.0135.2	151.068				
1	1138.37322.8270.5	122.136	162.136			

1	1237.73300.3267.5	132.136	172.136
1	1338.37305.9270.5	142.136	182.136
1	1438.37305.9270.5	152.136	192.136
1	1519.18153.0135.2	201.068	
1	1619.18153.0135.2	172.136	
1	1738.37305.9270.5	182.136	212.136
1	1838.37305.9270.5	192.136	222.136
1	1938.37305.9270.5	202.136	232.136
1	2019.18153.0135.2	241.068	
1	2119.18153.0135.2	222.136	
1	2238.37305.9270.5	232.136	252.136
1	2338.37305.9270.5	242.136	262.136
1	2419.18153.0135.2	271.068	
1	2519.18153.0135.2	262.136	
1	2638.37305.9270.5	272.136	282.136
1	2719.18153.0135.2	291.068	
1	2819.18153.0135.2	292.136	
1	2919.18153.0135.2	301.068	
1	304.79638.2433.81		

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.995		1										

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 211.565  
 221.565  
 231.565  
 241.565  
 251.565  
 261.565  
 271.565  
 281.565  
 291.565  
 301.565

	8	33	33	4	2	2	
1	1	.4221.366		1.2772		12.7700	
1	2	.4221.416		1.2772		2.2567	12.5133
1	3	.4221.465		1.2772		3.2567	12.5133
1	4	.4221.480		1.1492		2.1391	3.1381
1	5	.4221.472		2.2772		4.2772	12.5133
							4.1381

1	6	.4221.457	3.2772	12.7700
1	7	.4221.424	4.2772	12.7700
1	8	.422.6931	5209.4	
1	9	.422.7690	6104.7	
1	10	.422.7366	7209.4	
1	11	.4221.012	8209.4	
1	12	.4221.201	9209.4	
1	13	.422.8788	10104.7	
1	14	.422.7895	11209.4	
1	15	.4221.239	12205.6	
1	16	.422.9347	13209.4	
1	17	.4221.016	14209.4	
2	18	.4221.023	15104.7	
1	19	.4221.062	16104.7	
1	20	.4221.178	17209.4	
1	21	.4221.158	18209.4	
1	22	.4221.157	19209.4	
1	23	.422.9281	20104.7	
1	24	.422.9491	21104.7	
1	25	.422.9730	22209.4	
1	26	.422.9850	23209.4	
1	27	.4221.088	24104.7	
1	28	.4221.103	25104.7	
1	29	.4221.117	26209.4	
1	30	.422.8447	27104.7	
1	31	.422.9258	28104.7	
1	32	.4221.026	29104.7	
1	33	.422.F026	3026.18	
1.649	.0789660	.1.3835	1.50	.12494.4-01651000.
1.809	.0789660	.1.3880	7.58	.0806410.2.02401000.
	9	1	0	0
	.5	0.126.7	0.	21 0 0. 30 .010 .250
	10	2	0	0
.0062	-0.1			
	11	1	0	
	1972.	522.3	2.170334	.1694937
	12	3	0	3
1	4	5		

Sample Output for COBRA III C

Since there has been no change made in the output of the original version of COBRA III C, no sample output is given in this work. For further details, the reader is referred to Ref. 13.



## APPENDIX C

### COBRA III C CONNECTICUT YANKEE VERSION

#### C.1 Summary of the Changes Made in COBRA III C

The original version of COBRA III C, as it has been set up (13) was too small to accommodate the Connecticut Yankee case. The extended version can treat a bigger problem size in terms of channels number, fuel rods number. However the number of possible axial nodes has been reduced to make the space required to run the code smaller. This has been proved not to be an undesirable change, since the sensitivity analysis developed on the axial node length showed that axial node of less than 6 in. did not improve the accuracy of results but only increased the computing time (see Table 5).

A comparison of the original version and the Connecticut Yankee version of COBRA III C is given below.

COBRA III C version	Original	Connect. Yankee
Flow channels number	15	30
Flow channels connections number	30	47
Fuel rods number	15	35
Fuel types number	2	3
Axial nodes number	60	30

Axial heat flux nodes number  
(inputs)

30

39

Important Remark: In the designation of the different parameters above, it is very important to recognize that:

- flow channel can be taken either as a flow subchannel or as a fuel assembly in which all or part of the constituting subchannels are lumped together as one flow channel,
- flow channel connection can be made by two interconnected subchannels, or by two interconnected fuel assemblies each of them represented by a flow channel or by a subchannel interconnected with a fuel assembly represented by a flow channel,
- fuel rod can be taken as a physical fuel rod as it exists, or as an hypothetical fuel rod representing lumped fuel rods when a fuel assembly (or part of it) is represented as a flow channel.

## C.2 Procedure to Vary the Size of the Code

The remaining part of this section lists the changes made and tells a future user how to handle a change in the code as a function of the main code parameters.

The logic of the code has not been changed, only the size of some of the arrays has been altered.

The changes made are explained for each case:

- the cards are listed in the order they appear in the code (main program and then the subroutines or functions),
- in each section of the code the cards are listed with their number,
- for each card only the altered arrays are mentioned, with the new dimension used and the indication of the relation between this dimension and the code parameters (noted from 1 to 7).

Key for the following pages:

SUBROUTINE SCHEME	Name of the section of the code							
Card No	Array Name	1	2	3	4	5	6	7
0180	RHO(30,-), VPA(30)	x						
	RHO(-,31)					x		

In the subroutine SCHEME, the card number 0180 has been modified as the following:

- the array VPA is now dimensioned to 30 because it is related to the flow channel number (noted 1), and so does the array RHO for its first dimension,
- the second dimension of the array RHO is now 31 because it is related to the number of axial nodes (noted 5),

- 1 means the dimension depends on the flow channels number,
- 2 means the dimension depends on the flow channels connections number,
- 3 means the dimension depends on the fuel rods number,
- 4 means the dimension depends on the fuel types number,
- 5 means the dimension depends on the axial nodes number,
- 6 means the dimension depends on the axial heat flux nodes number,
- 7 means the dimension depends on the biggest parameter considered in the computation and indication is given on which parameter the dimension has been sized.

When an important part of the changes are identical to some made earlier in the code, reference is made to that part of the code to get the corresponding modifications. The number of the first and the last card defining a fraction of the code for which the changes have already been done, are inclusive.

MAIN PROGRAM

Card No.	Array Name	1	2	3	4	5	6	7
3110	FSPLIT(30)	x						
3160	V(30), VP(30), VISC(30), VISCW(30)	x						
	HFILM(30), CON(30)	x						
3170	CP(30), FSP(30), FMULT(30), U(30)	x						
	UH(30), ALPHA(30), QUAL(30)	x						
3180	RHO(30,-), VPA(30), T(30),	x						
	HINLET(30), FINLET(30)	x						
	RHO(-,31)					x		
3190	COND(47), WP(47), GAP(47), IK(47)		x					
	FACTOR(47)		x					
3200	JK(47), GAPN(47), LENGTH(47)		x					
	USTAR(47), W(47,-)		x					
	W(-,31)					x		
3210	A(30), AN(30), DHYD(30), DHYDN(30)	x						
	DFDX(30)	x						
3220	DHDX(30), DPDX(30), QPRIM(30)	x						
	PERIM(30)	x						
3230	HPERIM(30), NTYPE(30)	x						
3240	P(30,-), H(30,-), F(30,-)	x						
	P(-,31), H(-,31), F(-,31)					x		

MAIN PROGRAM

Card No.	Array Name	1	2	3	4	5	6	7
3250	WOLD(47,-)		x					
	WOLD(-,31), RHOOLD(-,31)					x		
	FOLD(-,31), HOLD(-,31)					x		
3250	RHOOLD(30,-), FOLD(30,-)	x						
	HOLD(30,-)	x						
3260	AXIAL(39), Y(39)						x	
	IDAREA(30)	x						
	IDGAP(47)		x					
3290	CD(30,-)	x						
3300	FXFLOW(47,-), FDIV(47)		x					
3400	LC(30,-), GAPS(30,-), AC(30), PW(30)	x						
		x						
3410	PH(30), DC(30), DIST(30,-) DR(35)	x			x			
3420	PRINTC(30)	x		x				
3430	PRINTR(35)			x				
3441	TINLET(30)	x						
3470	NWRAPS(30)	x						
3472	KFUEL(3), KCLAD(3), RFUEL(3) RCLAD(3)				x			
					x			
3473	CFUEL(3), CCLAD(3), TCLAD(3)				x			

MAIN PROGRAM

Card No.	Array Name	1	2	3	4	5	6	7
3474	FLUX(35,-), TROD(-,35,-)			x				
	LR(35,-)			x				
	FLUX(-,31), TROD(-,-,31)					x		
	HGAP(3)				x			
3475	PWRF(-,35), PHI(35,-),			x				
	RADIAL(35), D(35)			x				
	PWRF(30,-)	x						
3476	DFUEL(3)				x			
	IDFUEL(35)			x				
3480	XCROSS(47,-), DUR(47),		x					
	NWRAP(47)		x					
3490	SP(47,-)		x					
	SP(-,31)					x		
3491	CHFR(35,-), CCHANL(35,-)			x				
	CHFR(-,31), CCHANL(-,31),					x		
	MCHFR(31), MCHFRC(31),					x		
	MCHFRR(31)					x		
5400	MC = 30	x						
5420	MX = 31					x		
5440	MR = 35			x				

SUBROUTINE SCHEME

Card No.	Array Name	1	2	3	4	5	6	7
0110	FSPLIT(30)	x						
0160	V(30), VP(30), VISC(30), VISCW(30), HFILM(30), CON(30)	x						
0170	CP(30), FSP(30), FMULT(30), U(30), UH(30), ALPHA(30), QUAL(30)	x						
0180	RHO(30,-), VPA(30), T(30) HINLET(30), FINLET(30) RHO(-,31)	x					x	
0190	COND(47), WP(47), GAP(47) FACTOR(47), IK(47)		x					
0200	JK(47), GAPN(47), LENGTH(47) USTAR(47), W(47,-) W(-,31)		x					x
0210	A(30), AN(30), DHYD(30), DHYDN(30), DFDX(30)	x						
0220	DHDX(30), DPDX(30), QPRIM(30) PERIM(30)	x						
0230	HPERIM(30), NTYPE(30)	x						



SUBROUTINE SCHEME

Card No.	Array Name	1	2	3	4	5	6	7
0240	P(30,-), H(30,-), F(30,-)	x						
	P(-,31), H(-,31), F(-,31)					x		
0250	WOLD(47,-)		x					
	WOLD(-,31), RHOOLD(-,31)					x		
	FOLD(-,31), HOLD(-,31)					x		
	RHOOLD(30,-), FOLD(30,-)	x						
	HOLD(30,-)	x						
0260	AXIAL(39), Y(39)						x	
	IDAREA(30)	x						
	IDGAP(47)		x					
0290	CD(30,-)	x						
0300	FXFLOW(47,-), FDIV(47)		x					
0340	KFUEL(3), KCLAD(3), RFUEL(3)				x			
	RCLAD(3)				x			
0350	CFUEL(3), CCLAD(3), TCLAD(3)				x			
0360	FLUX(35,-), TROD(-,35,-), LR(35,-)			x				
	FLUX(-,31), TROD(-,-,31)					x		
	HGAP(3)				x			
0370	PWRF(-,35), PHI(35,-), RADIAL(35)			x				
	D(35)			x				
	PWRF(30,-)	x						

SUBROUTINE SCHEME

Card No.	Array Name	1	2	3	4	5	6	7
0380	DFUEL(3)				x			
	IDFUEL(35)			x				
0390	WSAVE(47)		x					
0400	SP(47,-)		x					
	SP(-,31)					x		

SUBROUTINE HEAT

Card No.	Array Name	1	2	3	4	5	6	7
0110	FSPLIT(30)	x						
0160	V(30), VP(30), VISC(30), VISCW(30), HFILM(30), CON(30)	x						
0170	CP(30), FSP(30), FMULT(30), U(30), UH(30), ALPHA(30), QUAL(30)	x						
0180	RHO(30,-), VPA(30), T(30) HINLET(30), FINLET(30) RHO(-,31)	x					x	
0190	COND(47), WP(47), GAP(47), IK(47)		x					
0190	FACTOR(47)		x					

SUBROUTINE HEAT

Card No.	Array Name	1	2	3	4	5	6	7
0200	JK(47), GAPN(47), LENGTH(47)		x					
	USTAR(47), W(47,-)		x					
	W(-,31)					x		
0210	A(30), AN(30), DHYD(30),	x						
	DHYDN(30), DFDX(30)	x						
0220	DHDX(30), DPDX(30), QPRIM(30)	x						
	PERIM(30)	x						
0230	HPERIM(30), NTYPE(30)	x						
0240	P(30,-), H(30,-), F(30,-)	x						
	P(-,31), H(-,31), F(-,31)					x		
0250	WOLD(47,-)		x					
	WOLD(-,31), RHOOLD(-,31)					x		
	FOLD(-,31), HOLD(-,31)					x		
	RHOOLD(30,-), FOLD(30,-)	x						
	HOLD(30,-)	x						
0260	AXIAL(39), Y(39)						x	
	IDAREA(30)	x						
	IDGAP(47)		x					
0290	CD(30,-)	x						
0300	FXFLOW(47), FDIV(47)		x					

SUBROUTINE HEAT

Card No.	Array Name	1	2	3	4	5	6	7
0350	KFUEL(3), KCLAD(3), RFUEL(3) RCLAD(3)				x			
0360	CFUEL(3), CCLAD(3), TCLAD(3)				x			
0370	FLUX(35,-), TROD(-,35,-), LR(35,-) FLUX(-,31), TROD(-,-,31) HGAP(3)			x			x	
0380	PWRF(-,35), PHI(35,-), RADIAL(35), D(35) PWRF(30,-)	x		x				
0390	DFUEL(3) IDFUEL(35)				x			

SUBROUTINE TEMP

Card No.	Array Name	1	2	3	4	5	6	7
0130	KFUEL(3), KCLAD(3), RFUEL(3) RCLAD(3)				x			
0140	CFUEL(3), CCLAD(3), TCLAD(3)				x			
0150	FLUX(35,-), TROD(-,35,-), LR(35,-) FLUX(-,31), TROD(-,-,31) HGAP(3)			x			x	

SUBROUTINE TEMP

Card NO.	Array Name	1	2	3	4	5	6	7
0160	PWRF(-,35), PHI(35,-), RADIAL(35)			x				
	D(35)			x				
	PWRF(30,-)	x						
0170	DFUEL(3)				x			
	IDFUEL(35)			x				

SUBROUTINE HCOOL

Card No.	Array Name	1	2	3	4	5	6	7
0090	FSPLIT(30)	x						
0140	V(30), VP(30), VISC(30), VISCW(30), HFILM(30), CON(30)	x						
		x						
0150	CP(30), FSP(30), FMULT(30), U(30), UH(30), ALPHA(30), QUAL(30)	x						
		x						
		x						
0160	RHO(30,-), VPA(30), T(30) HINLET(30), FINLET(30) RHO(-,31)	x						
		x						
						x		
0170	COND(47), WP(47), GAP(47) FACTOR(47), IK(47)		x					
			x					
0180	JK(47), GAPN(47), LENGTH(47) USTAR(47), W(47,-)		x					
			x					

SUBROUTINE HCOOL

Card No.	Array Name	1	2	3	4	5	6	7
0180	W(-,31)					x		
0190	A(30), AN(30), DHYD(30), DHYDN(30), DFDX(30)	x						
0200	DHDX(30), DPDX(30), QPRIM(30) PERIM(30)	x						
0210	HPERIM(30), NTYPE(30)	x						
0220	P(30,-), H(30,-), F(30,-) P(-,31), H(-,31), F(-,31)	x					x	
0230	WOLD(47,-) WOLD(-,31), RHOOLD(-,31) FOLD(-,31), HOLD(-,31)		x				x	
0230	RHOOLD(30,-), FOLD(30,-) HOLD(30,-)	x						
0240	AXIAL(39), Y(39) IDAREA(30) IDGAP(47)						x	
0270	CD(30,-)	x						
0280	FXFLOW(47,-), FDIV(47)		x					
0350	KFUEL(3), KCLAD(3), RFUEL(3) RCLAD(3)					x		
						x		

SUBROUTINE HCOOL

Card No.	Array Name	1	2	3	4	5	6	7
0360	CFUEL(3), CCLAD(3), TCLAD(3)				x			
0370	FLUX(35,-), TROD(-,35,-), LR(35)			x				
	FLUX(-,31), TROD(-,-,31)			x				
	HGAP(3)				x			
0380	PWRF(-,35), PHI(35,-), RADIAL(35)			x				
	D(35)			x				
	PWRF(30,-)	x						
0390	DFUEL(3)				x			
	IDFUEL(35)			x				

SUBROUTINE CHF

Card No.	Array Name	1	2	3	4	5	6	7
0110	FSPLIT(30)	x						
0160	V(30), VP(30), VISC(30),	x						
	VISCW(30)	x						
0160	HFILM(30), CON(30)	x						
0170	CP(30), FSP(30), FMULT(30), U(30)	x						
	UH(30), ALPHA(30), QUAL(30)	x						
0180	RHO(30,-), VPA(30), T(30),	x						
	HINLET(30), FINLET(30)	x						
	RHO(-,31)					x		

SUBROUTINE CHF

Card No.	Array Name	1	2	3	4	5	6	7
0190	COND(47), WP(47), GAP(47)		x					
	FACTOR(47), IK(47)		x					
0200	JK(47), GAPN(47), LENGTH(47)		x					
	USTAR(47), W(47,-)		x					
	W(-,31)					x		
0210	A(30), AN(30), DHYD(30), DHYDN(30)	x						
	DFDX(30)	x						
0220	DHDX(30), DPDX(30), QPRIM(30)	x						
	PERIM(30)	x						
0230	HPERIM(30), NTYPE(30)	x						
0240	P(30,-), H(30,-), F(30,-)	x						
	P(-,31), H(-,31), F(-,31)					x		
0250	WOLD(47,-)		x					
	WOLD(-,31), RHOOLD(-,31)					x		
	FOLD(-,31), HOLD(-,31)					x		
	RHOOLD(30,-), FOLD(30,-)	x						
	HOLD(30,-)	x						
0260	AXIAL(39), Y(39)						x	
	IDAREA(30)	x						
	IDGAP(47)		x					
0290	CD(30,-)	x						



SUBROUTINE CHF

Card No.	Array Name	1	2	3	4	5	6	7
0300	FXFLOW(47,-), FDIV(47)		x					
0330	JBOIL(30)	x						
0340	KFUEL(3), KCLAD(3), RFUEL(3)				x			
	RCLAD(3)				x			
0350	CFUEL(3), CCLAD(3), TCLAD(3)				x			
0360	FLUX(35,-), TROD(-,35,-), LR(35,-)				x			
	FLUX(-,31), TROD(-,-,31)						x	
	HGAP(3)				x			
0370	PWRF(-,35), PHI(35,-), RADIAL(35)				x			
	D(35)				x			
	PWRF(30,-)	x						
0380	DFUEL(3)				x			
	IDFUEL(35)				x			
0390	CHFR(35,-), CCHANL(35,-)						x	
	MCHFR(31), MCHFRC(31), CHFR(-,31)						x	
	CCHANL(-,31)						x	
0400	MCHFRR(31)						x	

FUNCTION CHF1 AND CHF2

Card No.	Array Name	1	2	3	4	5	6	7
0014	FSPLIT(30)	x						
0019	V(30), VP(30), VISC(30),	x						
	VISCW(30), HFILM(30), CON(30)	x						
0020	CP(30), FSP(30), FMULT(30),	x						
	U(30), UH(30), ALPHA(30),	x						
	QUAL(30)	x						
0021	RHO(30,-), VPA(30), T(30)	x						
	HINLET(30), FINLET(30)	x						
	RHO(-,31)						x	
0022	COND(47), WP(47), GAP(47)		x					
	FACTOR(47), IK(47)		x					
0023	JK(47), GAPN(47), LENGTH(47)		x					
	USTAR(47), W(47,-)		x					
	W(-,31)						x	
0024	A(30), AN(30), DHYD(30),	x						
	DHYDN(30), DFDX(30)	x						
0025	DHDX(30), DPDX(30), QPRIM(30)	x						
	PERIM(30)	x						
0026	HPERIM(30), NTYPE(30)	x						

FUNCTION CHF1 AND CHF2

Card No.	Array Name	1	2	3	4	5	6	7
0027	P(30,-), H(30,-), F(30,-)	x						
	P(-,31), H(-,31), F(-,31)					x		
0028	WOLD(47,-)		x					
	WOLD(-,31), RHOOLD(-,31)					x		
	FOLD(-,31), HOLD(-,31)					x		
0028	RHOOLD(30,-), FOLD(30,-)	x						
	HOLD(30,-)	x						
0029	AXIAL(39), Y(39)						x	
	IDAREA(30)	x						
	IDGAP(47)		x					
0032	CD(30,-)	x						
0036	JBOIL(30)	x						
0037	KFUEL(3), KCLAD(3), RFUEL(3)				x			
	RCLAD(3)				x			
0038	CFUEL(3), CCLAD(3), TCLAD(3)				x			
0039	FLUX(35,-), TROD(-,35,-),			x				
	LR(35,-)			x				
	FLUX(-,31), TROD(-,-,31)					x		
	HGAP(3)				x			

FUNCTION CHF1 AND CHF2

Card No.	Array Name	1	2	3	4	5	6	7
0040	PWRF(-,35), PHI(35,-), RADIAL(35), D(35)			x				
	PWRF(30,-)	x						
0041	DFUEL(3)				x			
	IDFUEL(35)			x				

SUBROUTINE DIFFER

Card No.	Array Name	1	2	3	4	5	6	7
0070	FSPLIT(30)	x						
0120	V(30), VP(30), VISC(30), VISCW(30)	x						
		x						
0120	HFILM(30), CON(30)	x						
0130	CP(30), FSP(30), FMULT(30), U(30)	x						
	UH(30), ALPHA(30), QUAL(30)	x						
0140	RHO(30,-), VPA(30), T(30)	x						
	HINLET(30), FINLET(30)	x						
	RHO(-,31)					x		
0150	COND(47), WP(47), GAP(47)		x					
	FACTOR(47), IK(47)		x					
0160	JK(47), GAPN(47), LENGTH(47)		x					

SUBROUTINE DIFFER

Card No.	Array Name	1	2	3	4	5	6	7
0160	USTAR(47), W(47,-)		x					
	W(-,31)					x		
0170	A(30), AN(30), DHYD(30),	x						
	DHYDN(30), DFDX(30)	x						
0180	DHDX(30), DPD(30), QPRIM(30)	x						
	PERIM(30)	x						
0190	HPERIM(30), NTYPE(30)	x						
0200	P(30,-), H(30,-), F(30,-)	x						
	P(-,31), H(-,31), F(-,31)					x		
0210	WOLD(47,-)		x					
	WOLD(-,31), RHOOLD(-,31)					x		
	FOLD(-,31), HOLD(-,31)					x		
	RHOOLD(30,-), FOLD(30,-)	x						
	HOLD(30,-)	x						

SUBROUTINE DIFFER

Card No.	Array Name	1	2	3	4	5	6	7
0220	AXIAL(39), Y(39)						x	
	IDAREA(30)	x						
	IDGAP(47)		x					

SUBROUTINE DIFFER

Card No.	Array Name	1	2	3	4	5	6	7
0250	CD(30,-)	x						
0260	FXFLOW(47,-), FDIV(47)		x					
0290	DPK(30)	x						

SUBROUTINE DIVERT

Card No.	Array Name	1	2	3	4	5	6	7
0070								
0120	Same changes as in Subroutine DIFFER, corresponding to the same cards numbers.							
0250								
0260								
0290	AAA(47,47), ANSWER(47), B(47)		x					x
	IPS(47)		x					x
0300	SP(47,-)		x					
	SP(-,31)		x					
0310	DPK(30)	x						
0320	USAVE(47)		x					x

SUBROUTINE PROP

Card No.	Array Name	1	2	3	4	5	6	7
0070								
0120	Same changes as in Subroutine							
0250	DIFFER, corresponding to the same							
0260	cards numbers.							
0285	JBOIL(30)	x						

SUBROUTINE VOID

Card No.	Array Name	1	2	3	4	5	6	7
0050	FSPLIT(30)	x						
0100	V(30), VP(30), VISC(30),	x						
	VISCW(30), HFILM(30), CON(30)	x						
0110	CP(30), FSP(30), FMULT(30), U(30)	x						
	UH(30), ALPHA(30), QUAL(30)	x						
0120	RHO(30,-), VPA(30), T(30)	x						
	HINLET(30), FINLET(30)	x						
	RHO(-,31)					x		
0130	COND(47), WP(47), GAP(47)		x					
	FACTOR(47), IK(47)		x					

SUBROUTINE VOID

Card No.	Array Name	1	2	3	4	5	6	7
0140	JK(47), GAPN(47), LENGTH(47)		x					
	USTAR(47), W(47,-)		x					
	W(-,31)					x		
0150	A(30), AN(30), DHYD(30),	x						
	DHYDN(30)	x						
0150	DFDX(30)	x						
0160	DHDX(30), DPDX(30), QPRIM(30)	x						
	PERIM(30)	x						
0170	HPERIM(30), NTYPE(30)	x						
0180	P(30,-), H(30,-), F(30,-)	x						
	P(-,31), H(-,31), F(-,31)					x		
0190	WOLD(47,-)		x					
	WOLD(-,31), RHOOLD(-,31)					x		
	FOLD(-,31), HOLD(-,31)					x		
	RHOOLD(30,-), FOLD(30,-)	x						
	HOLD(30,-)	x						
0200	AXIAL(39), Y(39)							x
	IDAREA(30)	x						
	IDGAP(47)		x					



SUBROUTINE VOID

Card No.	Array Name	1	2	3	4	5	6	7
0230	CD(30,-)	x						
0240	FXFLOW(47,-), FDIV(47)		x					
0270	PHI(30)	x						

SUBROUTINE MIX

Card No.	Array Name	1	2	3	4	5	6	7
0070	Same changes as in Subroutine							
	DIFFER, corresponding to the same							
0260	cards numbers ↓							

SUBROUTINE AREA

Card No.	Array Name	1	2	3	4	5	6	7
0070	↑							
0120	Same changes as in Subroutine							
	DIFFER, corresponding to the same							
0250	cards numbers.							
0260	↓							
0280	XCROSS(47,-), DUR(47), NWRAP(47)	x						

SUBROUTINE FORCE

Card No.	Array Name	1	2	3	4	5	6	7
0070	<hr style="width: 100px; margin: 0 auto;"/> ↑							
0120	Same changes as in Subroutine DIFFER, corresponding to the same							
0250	cards number.							
0260	↓ <hr style="width: 100px; margin: 0 auto;"/>							
0290	XCROSS(47,-), DUR(47), NWRAP(47)		x					

FUNCTION CIJ

Card No.	Array Name	1	2	3	4	5	6	7
0070	<hr style="width: 100px; margin: 0 auto;"/> ↑							
0120	Same changes as in Subroutine DIFFER, corresponding to the same							
0250	cards numbers.							
0260	↓ <hr style="width: 100px; margin: 0 auto;"/>							

SUBROUTINE SPLIT

Card No.	Array Name	1	2	3	4	5	6	7
0070	<hr style="width: 100px; margin: 0 auto;"/> ↑							

SUBROUTINE SPLIT

Card No.	Array Name	1	2	3	4	5	6	7
0120	Same changes as in Subroutine DIFFER, corresponding to the same cards numbers. ↓ _____ ↓							
0250								
0260								
0290		DPK(30)	x					

FUNCTION S

Card No.	Array Name	1	2	3	4	5	6	7
0070	_____ ↑ Same changes as in Subroutine DIFFER, corresponding to the same cards numbers. ↓ _____ ↓							
0120								
0250								
0260								

FUNCTION SCQUAL

Card No.	Array Name	1	2	3	4	5	6	7
0070	_____ ↑ Same changes as in Subroutine DIFFER, corresponding to the same cards numbers. ↓ _____ ↓							
0120								
0250								
0260								

FUNCTION BVOID

Card No.	Array Name	1	2	3	4	5	6	7
0060	FSPLIT(30)	x						
0110	V(30), VP(30), VISC(30), VISCW(30), HFILM(30), CON(30)	x x						
0120	CP(30), FSP(30), FMULT(30), U(30) UH(30), ALPHA(30), QUAL(30)	x x						
0130	RHO(30,-), VPA(30), T(30) HINLET(30), FINLET(30) RHO(-,31)	x x					x	
0140	COND(47), WP(47), GAP(47) FACTOR(47), IK(47)		x x					
0150	JK(47), GAPN(47), LENGTH(47) USTAR(47), W(47,-) W(-,31)		x x				x	
0160	A(30), AN(30), DHYD(30), DHYDN(30), DFDX(30)	x x						
0170	DHDX(30), DPDX(30), QPRIM(30) PERIM(30)	x x						
0180	HPERIM(30), NTYPE(30)	x						
0190	P(30,-), H(30,-), F(30,-) P(-,31), H(-31), F(-,31)	x					x	

FUNCTION BVOID

Card No.	Array Name	1	2	3	4	5	6	7
0200	WOLD(47,-)		x					
	WOLD(-,31), RHOOLD(-,31)					x		
	FOLD(-,31), HOLD(-,31)					x		
0200	RHOOLD(30,-), FOLD(30,-)	x						
	HOLD(30,-)	x						
0210	AXIAL(39), Y(39)						x	
	IDAREA(30)	x						
	IDGAP(47)		x					
0240	CD(30,-)	x						
0250	FXFLOW(47,-), FDIV(47)		x					

SUBROUTINE DECOMP

Card No.	Array Name	1	2	3	4	5	6	7
0040	UL(47,47), X(47), B(47), IPS(47)		x					x
0050	SCALES(47)		x					x

SUBROUTINE SOLVE

Card No.	Array Name	1	2	3	4	5	6	7
0020	UL(47,47), X(47), B(47), IPS(47)		x					x

SUBROUTINE CURVE

Card No.	Array Name	1	2	3	4	5	6	7
0020	F(47), Y(47)	-	x	-	-	-	-	x

APPENDIX D  
NOMENCLATURE

Letters	Explanation
$C_p$	Heat capacity of the coolant
D	Hydraulic diameter
$EFF_{1,j}$	Effective flow factor for the assembly of coordinates 1,j
f	friction factor
$f_G$	geometric factor
$f_p$	fraction of power
$F_{\Delta H}^E$	Enthalpy rise engineering subfactor
$F_H^N$	Enthalpy rise nuclear subfactor
$F_H^{stat}$	Enthalpy rise statistical subfactor
$F_{LP}$	Low plenum factor
$F_M$	Mixing factor
$F_o^E$	Heat flux engineering subfactor
$F_o^N$	Heat flux nuclear subfactor
$F_R$	Flow redistribution factor
$F_z$	Axial factor

Letters	Explanation
$h$	enthalpy
$\Delta h$	enthalpy difference
$k$	normalization factor (Eq. 2.6)
$k_t$	normalization factor (Eq. 2.10)
$m$	mass flow
$N_{rod}$	number of rods
$\sigma_{i,j}$	normalized power of the assembly of coordinates $i,j$
$Q_{i,j}$	energy generated by the assembly of coordinates $i,j$
$(\alpha/A)_1$	Heat flux for incipient boiling
$Re$	Reynolds number
$S$	Gap spacing between rods
$S/L$	Parameter defining the control volume
$t$	temperature
$\Delta t$	temperature difference
$T_w$	Wall temperature
$T_{sat}$	Saturation temperature
 Greek Letters	
$\alpha$	Fraction of power generated within the fuel
$\beta$	Turbulent mixing factor



$\sigma$  Standard deviation  
 $\sigma_r$  Relative standard deviation

Subscripts

$i, j$  Coordinates of the assembly  
 $in$  Inlet  
 $ou$  Outlet or exit  
 $r$  relative

APPENDIX E

DERIVATION OF EQUATIONS CHAPTER 2

E.1 Derivation of Eq. 2.7, 2.8, 2.9 in Chapter 2

Starting with Eq. 2.5 and 2.6

$$EFF_{1,j} = \frac{q_{1,j}}{\Delta t_{1,j}} \times k \quad , \quad (2.5)$$

$$k = \frac{38}{\sum_1 \left( \frac{q_{1,j}}{\Delta t_{1,j}} \right)} \quad . \quad (2.6)$$

Recalling that for a function a such as:

$$a = f(b,c), \quad (E.1)$$

$$\sigma^2_a = \left( \frac{\partial a}{\partial b} \right)^2 \sigma^2_b + \left( \frac{\partial a}{\partial c} \right)^2 \sigma^2_c \quad . \quad (E.2)$$

We can express:

$$\sigma^2(\text{EFF}_{1,j}) = \left[ \frac{\partial \text{EFF}_{1,j}}{\partial k} \right]^2 \sigma^2_k + \left[ \frac{\partial \text{EFF}_{1,j}}{\partial a_{1,j}} \right]^2 \sigma^2_{a_{1,j}} + \left[ \frac{\partial \text{EFF}_{1,j}}{\partial \Delta t_{1,j}} \right]^2 \sigma^2_{\Delta t_{1,j}}, \quad (\text{E.3})$$

$$= \left[ \frac{a_{1,j}}{\Delta t_{1,j}} \right]^2 \sigma^2_k + \left[ \frac{k}{\Delta t_{1,j}} \right]^2 \sigma^2_{a_{1,j}} + \left[ \frac{k a_{1,j}}{\Delta t_{1,j}^2} \right]^2 \sigma^2_{\Delta t_{1,j}}, \quad (\text{E.4})$$

where:

$$\sigma^2_k = \left[ \frac{\partial k}{\partial \left[ \sum_1^{38} \left( \frac{a_{1,j}}{\Delta t_{1,j}} \right) \right]} \right]^2 \sigma^2 \left[ \sum_1^{38} \left( \frac{a_{1,j}}{\Delta t_{1,j}} \right) \right], \quad (\text{E.5})$$

with

$$\frac{\sigma_k}{\sigma \left[ \sum_1^{38} \left( \frac{a_{1,j}}{\Delta t_{1,j}} \right) \right]} = \frac{\sigma_k}{\sigma \left[ \sum_1^{38} \left( \frac{a_{1,j}}{\Delta t_{1,j}} \right) \right]} \times \frac{\sigma \left[ \sum_1^{38} \left( \frac{a_{1,j}}{\Delta t_{1,j}} \right) \right]}{\sigma \left[ \sum_1^{38} \left( \frac{a_{1,j}}{\Delta t_{1,j}} \right) \right]} \quad (\text{E.6})$$

$$= 1 \times \left( - \frac{38}{\left[ \sum_1^{38} \left( \frac{a_{1,j}}{\Delta t_{1,j}} \right) \right]^2} \right) \quad (\text{E.7})$$

$$= 1 \times \frac{-k}{\sum_1^{38} \left( \frac{a_{1,j}}{\Delta t_{1,j}} \right)} \quad (\text{E.8})$$

Now Eq. E.5 becomes:

$$\sigma^2_k = \left[ \frac{-k}{\sum_1^{38} \left( \frac{a_{1,j}}{\Delta t_{1,j}} \right)} \right]^2 \sigma^2 \left[ \sum_1^{38} \left( \frac{a_{1,j}}{\Delta t_{1,j}} \right) \right] \quad (\text{E.9})$$

Recalling that for a function:

$$y = \eta_1 + \eta_2 + \dots + \eta_n = \sum_{\ell=1}^n \eta_{\ell} \quad , \quad (\text{E.10})$$

we have

$$\begin{aligned} \sigma^2_y &= \sigma^2 \left[ \sum_{\ell=1}^n \eta_{\ell} \right] = \sigma^2 \eta_1 + \sigma^2 \eta_2 + \dots + \sigma^2 \eta_n \\ &= \sum_{\ell=1}^n \sigma^2 \eta_{\ell} \quad . \end{aligned} \quad (\text{E.11})$$

Therefore:

$$\sigma^2 \left[ \sum_1^{38} \left( \frac{q_{i,j}}{\Delta t_{i,j}} \right) \right] = \sum_1^{38} \sigma^2 \left( \frac{q_{i,j}}{\Delta t_{i,j}} \right) \quad . \quad (\text{E.12})$$

Putting Eq. E.9, E.12 into Eq. E.4 gives:

$$\sigma^2(\text{EFF}_{i,j}) = \left( \frac{q_{i,j}}{\Delta t_{i,j}} \right)^2 \frac{k^2}{\left[ \sum_1^{38} \left( \frac{q_{i,j}}{\Delta t_{i,j}} \right) \right]^2} \sum_1^{38} \sigma^2 \left( \frac{q_{i,j}}{\Delta t_{i,j}} \right) \quad (\text{E.13})$$

$$+ \left( \frac{k}{\Delta t_{i,j}} \right)^2 \sigma^2_{\alpha_{i,j}} + \left( \frac{k \alpha_{i,j}}{\Delta t_{i,j}^2} \right)^2 \sigma^2_{\Delta t_{i,j}} \quad \text{(E.13)}$$

(continued)

Using Eq. 2.1 we may have:

$$\Delta t_{i,j} = t_{ou,i,j} - t_{in,i,j} \quad , \quad \text{(2.1)}$$

and

$$\sigma^2_{\Delta t_{i,j}} = \sigma^2_{t_{ou,i,j}} + \sigma^2_{t_{in,i,j}} \quad \text{(E.14)}$$

We could also express:

$$\sigma^2_{\alpha_{i,j}} = (\sigma_r \alpha_{i,j})^2 \alpha_{i,j}^2 \quad \text{(E.15)}$$

Using Eq. E.14, E.15 in Eq. E.13 gives Eq. 2.8:

$$\begin{aligned}
\sigma^2(\text{EFF}_{1,j}) &= \left( \frac{q_{1,j}}{\Delta t_{1,j}} \right)^2 \frac{k^2}{\left[ \sum_1^{38} \left( \frac{q_{1,j}}{\Delta t_{1,j}} \right) \right]^2} \sum_1^{38} \sigma^2 \left( \frac{q_{1,j}}{\Delta t_{1,j}} \right) \\
&+ \left( \frac{k}{\Delta t_{1,j}} \right)^2 \left( \sigma_r^{q_{1,j}} \right)^2 q_{1,j}^2 \\
&+ \left( \frac{k q_{1,j}}{\Delta t_{1,j}^2} \right)^2 \sigma^2_{t_{ou,1,j}} + \left( \frac{k q_{1,j}}{\Delta t_{1,j}^2} \right)^2 \sigma^2_{t_{in,1,j}} \quad (2.8)
\end{aligned}$$

Now from Eq. E15 we may have:

$$\begin{aligned}
\sigma_r^2(\text{EFF}_{1,j}) &= \frac{\sigma^2(\text{EFF}_{1,j})}{\text{EFF}_{1,j}^2} \\
&= \frac{\left( \frac{q_{1,j}}{\Delta t_{1,j}} \right)^2 \frac{k^2}{\left[ \sum_1^{38} \left( \frac{q_{1,j}}{\Delta t_{1,j}} \right) \right]^2} \sum_1^{38} \sigma^2 \left( \frac{q_{1,j}}{\Delta t_{1,j}} \right)}{\left( \frac{q_{1,j}}{\Delta t_{1,j}} \right)^2 k^2} \quad (E.16)
\end{aligned}$$

$$+ \frac{\frac{k^2}{\Delta t_{1,j}^2} (\sigma_r q_{1,j})^2 q_{1,j}^2 + \frac{k^2 \sigma_{1,j}^2}{\Delta t_{1,j}^4} \sigma_{t_{ou,1,j}}^2 + \frac{k^2 \sigma_{1,j}^2}{\Delta t_{1,j}^4} \sigma_{t_{in,1,j}}^2}{\left(\frac{q_{1,j}}{\Delta t_{1,j}}\right)^2 k^2}$$

(E.16)  
(continued)

This leads after simplification to Eq. 2.7

$$\sigma_r^2 (\text{EFF}_{1,j})$$

$$= \frac{\sum_1^{38} \sigma^2 \left[ \frac{q_{1,j}}{\Delta t_{1,j}} \right]}{\left[ \sum_1^{38} \left( \frac{q_{1,j}}{\Delta t_{1,j}} \right) \right]^2} + \sigma_r^2 q_{1,j}$$

$$+ \frac{\sigma_{t_{ou,1,j}}^2}{\Delta t_{1,j}^2} + \frac{\sigma_{t_{in,1,j}}^2}{\Delta t_{1,j}^2} \quad (2.7)$$



Recalling the fact that for a function

$$a = \frac{b}{c} , \quad (E.17)$$

$$\sigma^2 a = a^2 \left[ \frac{\sigma^2 b}{b^2} + \frac{\sigma^2 c}{c^2} \right] , \quad (E.18)$$

we can express Eq. E.12 as:

$$\begin{aligned} \sigma^2 \left[ \sum_1^{38} \left( \frac{q_{1,j}}{\Delta t_{1,j}} \right) \right] &= \sum_1^{38} \sigma^2 \left[ \frac{q_{1,j}}{\Delta t_{1,j}} \right] \\ &= \sum_1^{38} \left[ \frac{q_{1,j}}{\Delta t_{1,j}} \right]^2 \left[ \frac{\sigma^2 q_{1,j}}{q_{1,j}^2} + \frac{\sigma^2 \Delta t_{1,j}}{\Delta t_{1,j}^2} \right] . \end{aligned} \quad (E.19)$$

The first term of Eq. 2.8 can be expressed using Eq. E.14, 19 as Eq. (2.9):

$$\left[ \frac{q_{1,j}}{\Delta t_{1,j}} \right]^2 \frac{k^2}{\left[ \sum_1^{38} \left( \frac{q_{1,j}}{\Delta t_{1,j}} \right) \right]^2} \sum_1^{38} \sigma^2 \left[ \frac{q_{1,j}}{\Delta t_{1,j}} \right] \quad (2.9)$$

$$= \left[ \frac{q_{1,j}}{\Delta t_{1,j}} \right]^2 \frac{k^2}{\left[ \sum_1^{38} \left( \frac{q_{1,j}}{\Delta t_{1,j}} \right) \right]^2}$$

$$\times \sum_1^{38} \left[ \frac{q_{1,j}}{\Delta t_{1,j}} \right]^2 \left[ \sigma_r^2 q_{1,j} + \frac{\sigma_{t_{ou,1,j}}^2}{\Delta t_{1,j}^2} + \frac{\sigma_{t_{in,1,j}}^2}{\Delta t_{1,j}^2} \right]. \quad (2.9)$$

(continued)

## E.2 Derivation of Eq. 2.11, 2.12, 2.13 in Chapter 2

Equation 2.11 can be obtained from Eq. 2.7 by using  $\Delta h_{1,j}$  instead of  $\Delta t_{1,j}$ . Assuming Eq. 2.14 valid for sub-cooled coolant:

$$\sigma^2 h = \left[ \frac{\partial h}{\partial t} \right]^2 \sigma^2 t, \quad (2.14)$$

we may express:

$$\sigma^2 h_{ou,1,j} = \left[ \frac{\partial h_{ou,1,j}}{\partial t_{ou,1,j}} \right]^2 \sigma^2 t_{ou,1,j}, \quad (E.20)$$

$$\sigma^2_{h_{in,i,j}} = \left[ \frac{\partial h_{in,i,j}}{\partial t_{in,i,j}} \right]^2 \sigma^2_{t_{in,i,j}} \quad (E.21)$$

Equation 2.12 can be obtained from Eq. 2.18 by using:

-  $\sigma^2_{h_{ou,i,j}}$  instead of  $\sigma^2_{t_{ou,i,j}}$  ,

-  $\sigma^2_{h_{in,i,j}}$  instead of  $\sigma^2_{t_{in,i,j}}$  ,

and use Eq. E.20, E.21.

Equation E.13 is obtained from Eq. 2.9 by using the same procedure as above.