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# Structure-property relationships in metal-organic frameworks for hydrogen storage

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## **Abstract**

Experimental hydrogen isotherms on several metal-organic frameworks (IRMOF-1, IRMOF-3, IRMOF-9, ZIF-7, ZIF-8, ZIF-9, ZIF-11, ZIF-12, ZIF-CoNIm, MIL-101 (Cr), NH<sub>2</sub>-MIL-101 (Cr), NH<sub>2</sub>-MIL-101 (Al), UiO-66, UiO-67 and HKUST-1) synthesized in-house and measured at 77 K and pressures up to 18 MPa are presented, along with N<sub>2</sub> adsorption characterization. The experimental isotherms together with literature high pressure hydrogen data were analysed in order to search for relationships between structural properties of the materials and their hydrogen uptakes. The total hydrogen capacity of the materials was calculated from the excess adsorption assuming a constant density for the adsorbed hydrogen. The surface area, pore volumes and pore sizes of the materials were related to their maximum hydrogen excess and total hydrogen capacities. Results also show that ZIF-7 and ZIF-9 (SOD topology) have unusual hydrogen isotherm shapes at relatively low pressures, which is indicative of “breathing”, a phase transition in which the pore space increases due to adsorption. This work presents novel correlations using the modelled total hydrogen capacities of several MOFs. These capacities are more practically relevant for energy storage applications than the measured excess hydrogen capacities. Thus, these structural correlations will be advantageous for the prediction of the properties a MOF will need in order to meet the US Department of Energy targets for the mass

and volume capacities of on-board storage systems. Such design tools will allow hydrogen to be used as an energy vector for sustainable mobile applications such as transport, or for providing supplementary power to the grid in times of high demand. Keywords: hydrogen adsorption, nitrogen adsorption, hydrogen storage, MOF, structure-property relationship, breathing structure.

## **1. Introduction**

During the industrial revolution, humanity intensively used fossil fuels (mostly petroleum and coal in the beginning), which caused a rapid growth in population and economy, resulting in a corresponding increase in energy consumption. Today, coal, oil and natural gas are the primary energy sources used across the world, and their use has caused a continuous rise in CO<sub>2</sub> levels in the atmosphere (exceeding 400 ppm in January 2015) [1]. This increase in concentration of greenhouse gases is increasing the Earth's global temperature and predicts a rise in oceans' level, contributing to what is known as anthropogenic global warming [2]. It is predicted that energy consumption will carry on growing in the 21<sup>st</sup> century, creating a colossal challenge in the future, as societies will need to decarbonise their economies and replace increasingly scarce fossil fuel energies with clean renewable energies [3].

This switch represents major challenges in many areas and highlights the need for energy storage, due to the intermittence in production of renewable energies such as solar and wind power, to balance supply and demand in the national electricity grid. The transport sector is also one that needs to be decarbonised, as it was responsible for 13.1 % of all global emissions from 2004 and is almost completely reliant on oil [4].

Hydrogen shows great potential to be used as an energy vector due to its intrinsic characteristics. Among its benefits, hydrogen is the chemical fuel with the highest energy density by weight (after uranium and thorium), having a value of 142 MJ kg<sup>-1</sup>, which is about three times more energy than gasoline and seven times more than coal per unit mass [5-7]. Furthermore, hydrogen can be obtained from water, a very abundant resource, which is more readily accessible than fossil fuels. However, its energy density by unit volume is very low, presenting storage problems, particularly for mobile applications. Mature storage technologies include compressed and cryogenic hydrogen storage. However, their associated costs from compression and cooling respectively are a concern, as well as safety issues from storing hydrogen at high

pressures when compressed [8]. One possible solution is to use nanoporous materials to physically adsorb hydrogen, which reduces energy penalties by not requiring such low temperatures as liquefaction, and stores hydrogen at more moderate pressures than compression.

Among the materials that can be used as adsorbents there are metal-organic frameworks (MOFs), activated carbons, zeolites and porous polymers [5]. MOFs are crystalline materials formed by the connection of metal ions or clusters through organic molecules, which act as linkers. MOFs have open channels or cavities with sizes ranging from micro- to the meso-scale [9]. They show so far the highest hydrogen uptake and surface area among all adsorbents but the overall costs can be high, depending on the type of metal and linker used [10, 11]. The preparation of these materials is generally scalable, giving high yield, and by carefully choosing the building blocks, targeted MOFs can be created. They are usually synthesized using solvothermal methodologies at relatively mild conditions. Due to the crystallinity of these materials, powder X-ray diffraction can be used as an effective technique to determine the success of the synthesis [7, 12]. This peculiar type of material has become interesting for applications such as gas storage, separation, and catalysis due to its accessible surface area and permanent porosity. Therefore, this work aims to predict the hydrogen capacities of these materials based on their structural properties. A methodology previously developed at Bath is used to predict the total hydrogen capacity from the excess isotherms of several materials tested with hydrogen at high pressures [13, 14]. The physical characterisation of these materials, their maximum uptakes and their total hydrogen capacities have been examined to identify useful correlations between them. The maximum uptake correlations show similar correlations found in the past by other authors using measured excess uptake data. The total hydrogen capacity correlations however, result in a novel and more practical tool for determining the properties a MOF would need to have in order to meet the US DOE (US Department of Energy) targets, given the mass and volume of the tank, with the results having been compared across several different MOF families with different metal centres.

## 2. Background study

The existence of relationships between different adsorbents and hydrogen adsorption has been researched in the past. The first trends relating micropore volume and surface area with hydrogen uptake were observed by Chahine and Bénard using different microporous activated carbons [15, 16]. Materials were tested at 77 K at pressures up to 3.5 MPa, taking from the isotherms either the maximum uptake value or a value close to it for each of the tested materials. This led to the well-known “Chahine rule”, which states a linear correlation between variables, predicting an increase of 1 wt % per 500 m<sup>2</sup> g<sup>-1</sup> and a 1 wt % per 0.2 cm<sup>3</sup> g<sup>-1</sup>.

Panella and colleagues tested different microporous carbons at 77 K and RT: single-walled carbon nanotubes (SWCNTs), multi-walled carbon nanotubes MWCNTs, polyhedral nanoparticles and activated carbons [17]. In that report, the experimental data was fitted to a Langmuir-type equation (type I isotherm). The saturation value of each Langmuir fit for each material (denominated as the “storage capacity”) was used. The work of Panella et al. also indicated the existence of a linear dependence between BET surface area and pore volume at 77 K and RT with storage capacity. These findings show independence with the type of carbon nanostructure, concluding that high surface area and microporosity are desirable for high uptake materials. The maximum pressure of these isotherms (up to 7 MPa) was sometimes not high enough to fully determine the maximum excess uptake. This, combined with a limited number of isotherm points resulted in large error bars in some cases. Also, materials were degassed and heated at 200 °C for approximately 2 hours, which might have not been enough to remove all contaminants/He from the pores before testing them for hydrogen sorption. Gogotsi et al. investigated a large number of carbide-derived carbons (CDCs) with tuned surface area, pore volume and pore size in order to search for relationships between structural properties and hydrogen storage [18]. All the tests and analyses were done at 77 K and up to 6 MPa. A scattered relationship between hydrogen excess and surface area was found. If details of pore structure (size, shape etc.) were irrelevant, then capacity would be expected to vary linearly with surface area. Materials that outperformed the Chahine rule generally show a greater fraction of pores with diameter smaller than 1.5 nm and/or 0.7 nm median pore size in their pore size distributions (PSDs). Therefore, a graph of the excess capacity normalized per surface area of each material versus pore size experimentally showed which pore ranges were best for hydrogen storage. From the

correlation it was concluded that pores larger than 1.5 nm had little contribution to hydrogen storage. Pores of 0.6–0.7 nm in diameter provide the largest hydrogen uptake per unit of surface at elevated pressures and liquid nitrogen temperatures. The results also show that the effect of pore size is stronger than the effect of surface chemistry on the hydrogen uptake. This shows that Chahine rule is not universal, meaning that even if a material has a lower surface area than another, it may still have higher uptake if it has more pores of a smaller diameter [17, 18].

Thomas tested materials of different nature (carbon, silica, alumina, metal-organic frameworks and polymer porous materials) at 77 K and observed scattered linear trends for surface area (especially for surface areas higher than 1000 m<sup>2</sup> g<sup>-1</sup>) and pore volume. The work also showed that materials with microporous pore volumes lower than 0.8 g cm<sup>-3</sup> have a hydrogen density in their pores similar to that of liquid H<sub>2</sub> (0.0708 g cm<sup>-3</sup>). The hydrogen isotherm data used in these correlations was limited to 0.1 MPa, making it difficult to determine the maximum hydrogen excess accurately. Also, different methods for calculating pore structure characteristics (surface area and pore volume) such as surface areas obtained from BET and from t-method needed to be used [19]. Yaghi found an approximate linear correlation when plotting the maximum hydrogen uptake of several MOFs against their Langmuir surface area [20]. The same materials were used in this work because of their high pressure hydrogen isotherms, although BET surface area was used instead of Langmuir, since it assumes multilayer adsorption, while Langmuir assumes monolayer adsorption [20].

For this work, several MOFs from different classes were synthesized to look for relationships between hydrogen uptake, total hydrogen capacity and structural properties of the materials. MOFs were chosen because they show the highest hydrogen uptakes among adsorbents. The materials were tested with N<sub>2</sub> at 77 K to obtain their structural properties and with hydrogen at high pressures (up to 18 MPa), clearly showing their maximum excess points. Materials were degassed for periods between 6 and 8 h relying on Thermogravimetric analysis (TGA) to find the appropriate degassing temperature. Different framework topologies were used to look for differences among them and widen the validity of the correlation. This work also looked for consistency in the methodologies to calculate surface areas, pore volumes and pore sizes. However,

different methodologies from literature and experiments had to be used for total pore volume and pore size in order to be able to plot a reasonable number of data points.

Hydrogen adsorption excess isotherms in solid-state porous materials can be experimentally obtained but the total amount stored in a material, a quantity of more practical interest, cannot be measured directly using volumetric or gravimetric gas sorption techniques. Total adsorption, unlike excess uptake, takes into account all the hydrogen contained in the material, whether it is adsorbed or not. Adsorption thermodynamics are described by the spreading pressure and pressure tensor of the adsorptive, as well as the surface area of the material. Due to the complex geometry of porous materials, it is not possible to analyse the pressure tensor of the hydrogen [21]. Hence, a model needs to be used to predict the total hydrogen capacity of the materials, which is done here by fitting the excess hydrogen isotherms to a semi-empirical mathematical model, using a Type 1 isotherm. High pressures were needed to reach maximum excess uptake, which was necessary for obtaining reliable fits to the data for calculation of total hydrogen capacity. The maximum pressures for some hydrogen isotherms found in literature were insufficient, and thus resulted in greater uncertainties in the modelled total uptake. The total hydrogen capacity has been calculated by multiplying the pore volume by the density of the adsorbate obtained from the model fitting (which is assumed as constant for the different pressures and temperatures), assuming that the pore is completely filled with adsorbate (fractional filling  $\Theta$  equal to 1).

## **2. Materials and methods**

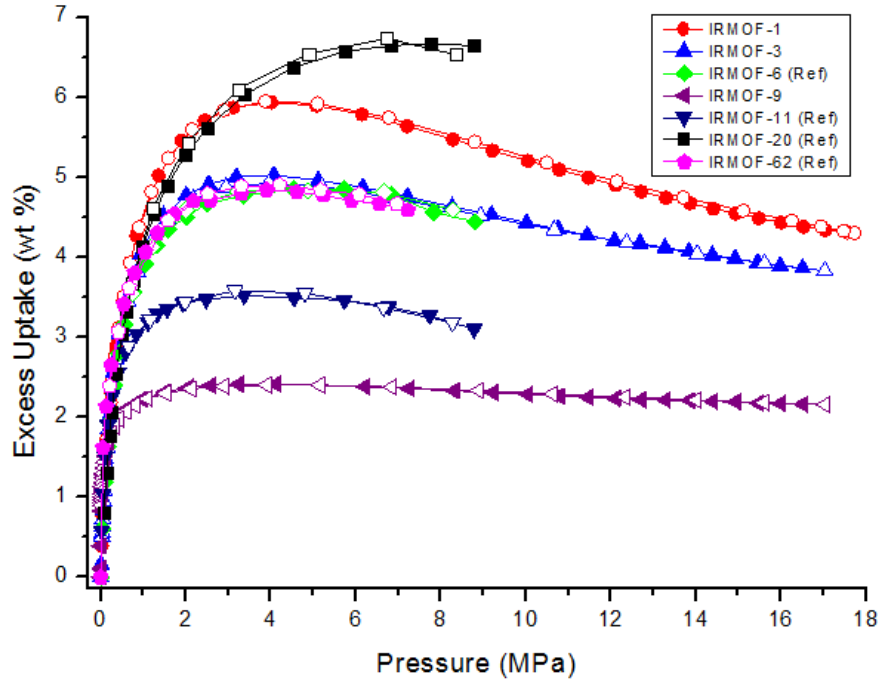
The materials were synthesised according to methods reported in the literature [22-29]. In some cases, the synthesis was scaled up or larger sample sizes were produced by combining multiple batches. HKUST-1 (Basolite<sup>TM</sup> C300) was supplied by Sigma Aldrich. A detailed explanation for the synthesis of all the tested can be found in the Supplementary Information. For Powder XRD measurements, a Bruker D8 Advance Diffractometer (Cu-K $\alpha$  radiation,  $\lambda = 1.54184 \text{ \AA}$ ) (Bruker, Billerica, US) with a lynxeye detector at 40 kV and 40 mA was used. A step size of  $0.041 \text{ }^\circ \text{ s}^{-1}$  ( $0.0081996 \text{ }^\circ \text{ step}^{-1}$  with a time per step of 0.2 seconds was chosen). Measurements were done in flat plate mode at 298 K on wet crystalline samples. XRD spectra were compared with the

original CIF files obtained from the Cambridge Crystallographic database and literature publications to ensure the materials were synthesized successfully. In order to investigate the thermal stability of the materials, a Setaram TGA 92 16.18 (Setaram, Caluire, France) was used. The materials were tested from 20 to 600 °C with a ramp rate of 5 °C min<sup>-1</sup> using N<sub>2</sub> as carrier gas. For pore size distributions, N<sub>2</sub> isotherms of the materials were measured at 77 K in a Micromeritics ASAP 2020 (Micromeritics Instrument Corporation, Georgia, USA). The method to calculate BET surface areas was consistent with the BS ISO 9277:2010, which uses the consistency criteria reported by Rouquerol [30, 31]. To obtain the microporous and total pore volume of the materials, Dubinin-Radushkevich (DR) and Horvath-Kawazoe (HK) methodologies were used [32, 33]. All these values were obtained using the MicroActive V 1.01 software supplied by Micromeritics. The hydrogen isotherms (77 K) were collected at equilibrium in a volumetric Hiden HTP-1 sorption analyser using a liquid nitrogen immersion dewar for temperature control (Hiden Isochema, Warrington, UK). The nonlinear fitting and calculations were done on OriginPro 9.1 (OriginLab, Northampton, Massachusetts, USA). The nonlinear fitting tool in Origin 9.1 is based on the Levenberg–Marquardt algorithm [34]. In order to assess the linear fittings, the standard deviation of the residuals (Root-MSE) has been used. Root-MSE has been used to assess linear fittings instead of R<sup>2</sup> since R<sup>2</sup> does not give a meaningful value to the fittings forced through the origin due to the elimination of the intercept.

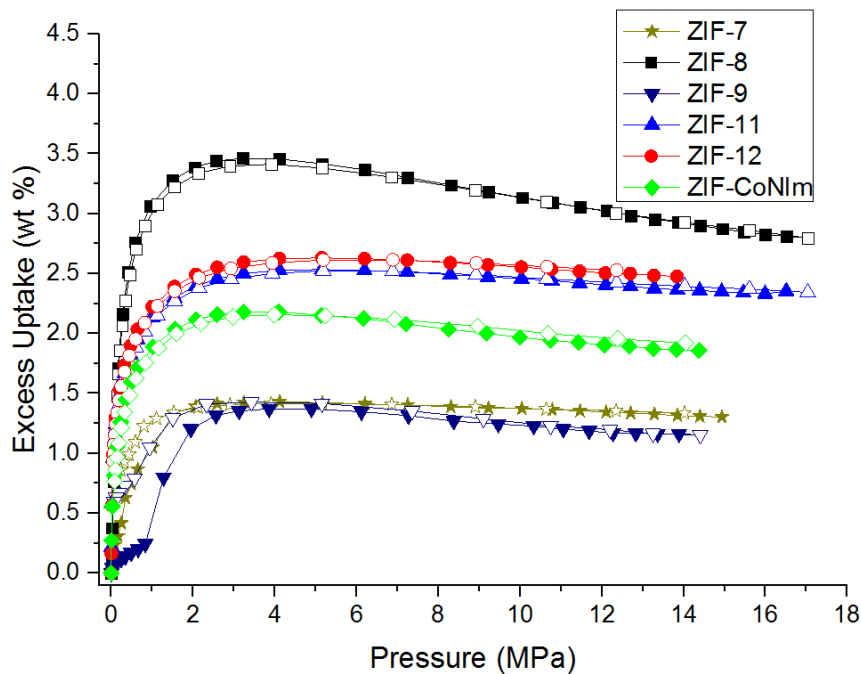
### **3. Results**

Hydrogen adsorption was measured on a wide range of metal-organic frameworks. Figures 1, 2, 3 and 4 show the hydrogen isotherms of all materials used in this work, grouped by topologies, where the excess H<sub>2</sub> uptake is in wt% with reference to the dry weight of the MOF adsorbent. Figure 4 shows the hydrogen isotherms of the UiOs, MOFs and HKUST-1. The stated data in the figures were obtained from literature (Supplementary Information files or Engauge Digitizer V.4.1) [20, 35].

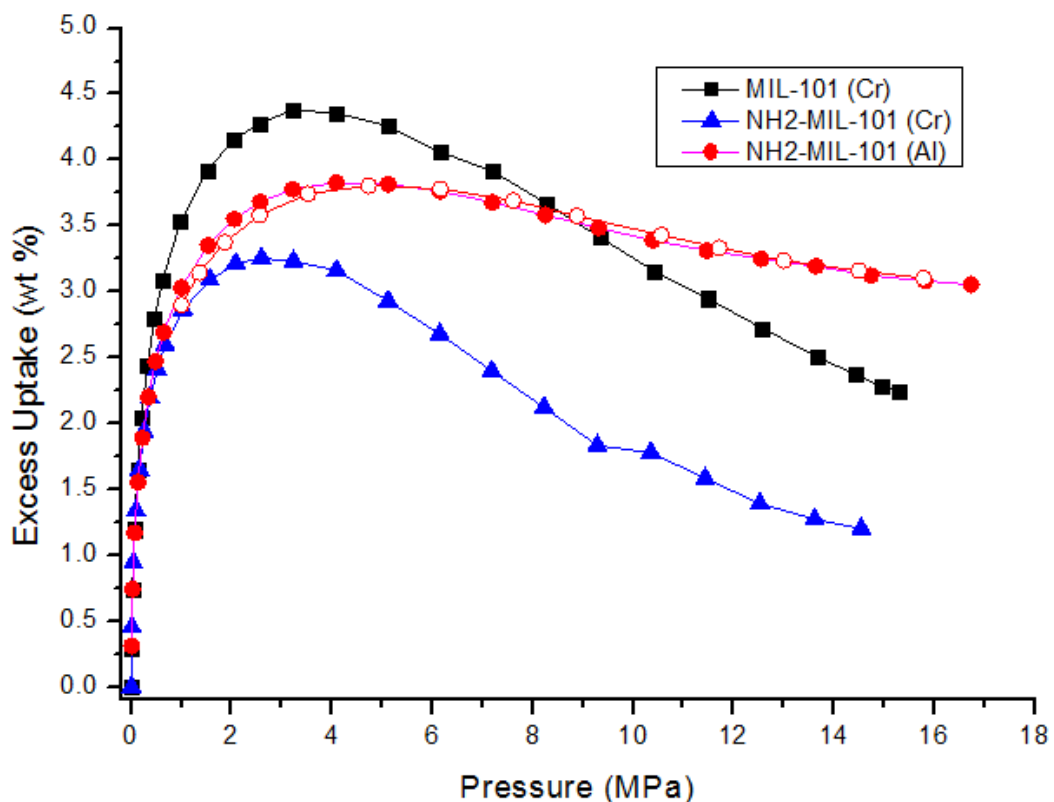




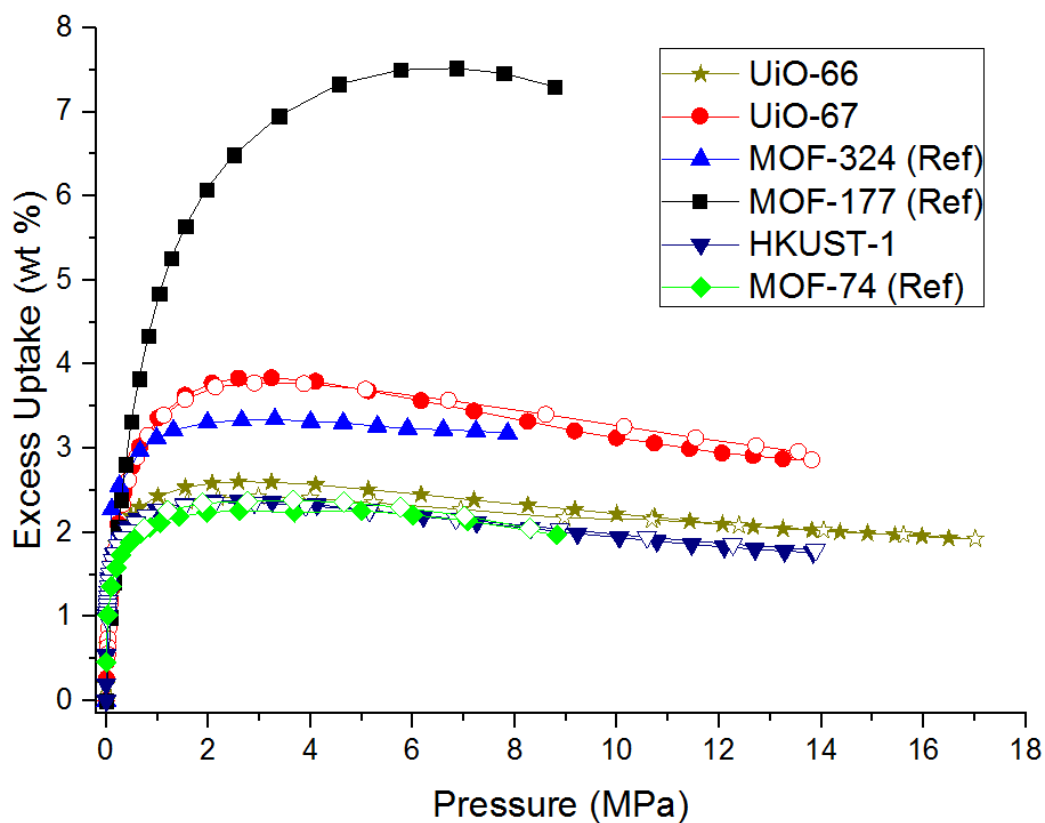
**Fig 1.** Excess hydrogen isotherms for the IRMOF family of materials at 77 K. Open symbols represent the desorption isotherms for each material. Data for IRMOF-6, IRMOF-11, IRMOF-20 and IRMOF-62 were taken from literature [20, 35].



**Fig 2.** Excess hydrogen isotherms for the ZIF family of materials at 77 K. Open symbols represent the desorption isotherms for each material.



**Fig 3.** Excess hydrogen isotherms for the MIL family materials at 77 K. Open symbols represent the desorption isotherms for each material.



**Fig 4.** Excess hydrogen isotherms for the UiOs, MOFs and HKUST-1 at 77 K. Open symbols represent the desorption isotherms for each material. Data for MOF-324, MOF-177 and MOF-74 were taken from literature [20, 35].

From Figures 1, 2, 3 and 4 the maximum excess uptake, used in the correlations, and its pressure for each material can be seen in Table 1:

**Table 1.** Maximum excess and pressure of materials.

<b>Material name</b>	<b>Pressure (MPa)</b>	<b>Maximum excess uptake (wt %)</b>	<b>Material name</b>	<b>Pressure (MPa)</b>	<b>Maximum excess uptake (wt %)</b>
<b>IRMOF-1</b>	4.01	5.93	<b>ZIF-7</b>	4.12	1.43
<b>IRMOF-3</b>	4.07	5.02	<b>ZIF-8</b>	3.22	3.46
<b>IRMOF-6</b>	4.53	4.85	<b>ZIF-9</b>	3.86	1.37
<b>IRMOF-9</b>	4.12	2.41	<b>ZIF-11</b>	5.15	2.53
<b>IRMOF-11</b>	3.37	3.52	<b>ZIF-12</b>	5.15	2.63
<b>IRMOF-20</b>	7.76	6.67	<b>ZIF-CoNIm</b>	3.23	2.18
<b>IRMOF-62</b>	3.9	4.84	<b>MIL-101 (Cr)</b>	3.20	4.38
<b>MOF-74</b>	4.99	2.26	<b>NH<sub>2</sub>-MIL-101 (Cr)</b>	2.59	3.25
<b>MOF-177</b>	6.85	7.52	<b>NH<sub>2</sub>-MIL-101 (Al)</b>	4.08	3.82
<b>MOF-324</b>	3.30	3.34	<b>UiO-66</b>	2.59	2.60
<b>HKUST-1</b>	2.60	2.38	<b>UiO-67</b>	3.23	3.84

Figure 2 shows the hydrogen isotherms for all the tested ZIFs. ZIFs 7 (Zn), ZIF-8 (Zn) and ZIF-9 (Co) possess SOD topology while ZIF-11 (Zn), ZIF-12 (Co) and ZIF-CoNIm (Co) possess RHO topologies. SOD topology is formed of cuboctahedral cages (known as beta cages). These cages are composed of 4 and 6 membered ring windows with 24 Co or Zn atoms per unit cell. Each  $\beta$  cage is connected to six other  $\beta$  cages by sharing double 4 membered ring units. It differs from the RHO topology, which is formed of  $\alpha$  cages (with 4, 6 and 8 membered windows, with 48 Zn or Co per unit cell) connected small polyhedral units (known as D8R) that link the  $\alpha$  cages with each other [36, 37]. Both ZIF-7 and ZIF-9 (SOD topologies) show unusual hydrogen isotherm shapes at

relatively low pressures. ZIF-7 has been reported to have a sorbate-induced gate-opening phenomena, involving a narrow-to-large pore phase transition [38-40]. This peculiar sorption pattern has been confirmed in CO<sub>2</sub> and C<sub>2</sub>-C<sub>4</sub> alkane/alkaline adsorption [40, 41]. Since ZIF-7 and ZIF-9 only differ in the nature of the metal cluster and both show special hydrogen isotherm shapes, it indicates that ZIF-9 may also show sorbate-induced gate-opening phenomena. Our results clearly show a feature that is indicative of the same phase transition from a narrow to large pore at 77 K and at 1 MPa.

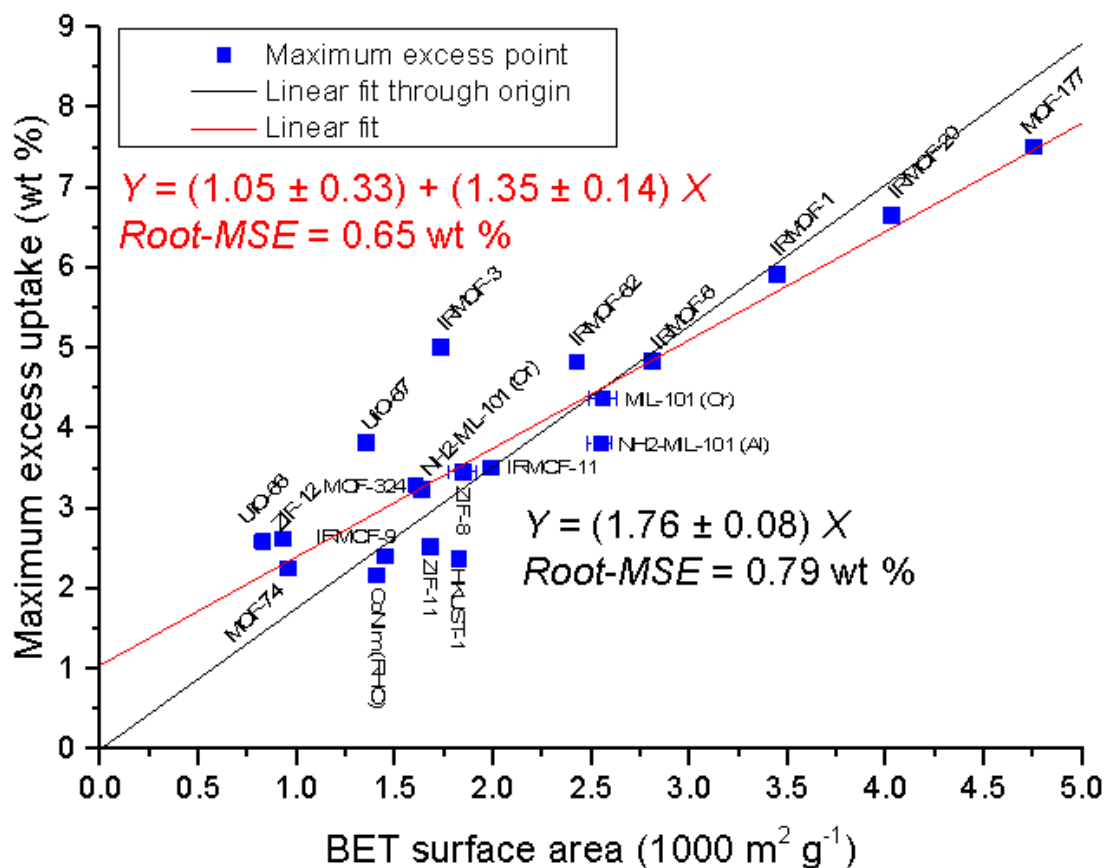
Also, the maximum hydrogen uptakes for ZIF-7 and ZIF-9 are very similar, having a value of 1.43 (at 4.12 MPa) and 1.37 (at 3.86 MPa) wt. % respectively. These values are also similar for their RHO homologues, as ZIF-11 and ZIF-12 show 2.53 and 2.63 wt % respectively, at the same pressure (5.15 MPa). This shows very similar maximum excess uptakes for both forms, showing that the nature of the metal (Co or Zn) does not have much influence on the hydrogen uptake of the material. Also, the maximum uptake difference between topologies is slightly less than double in both cases.

Figure 3 shows that, while MIL-101 (Cr) has a higher excess uptake, NH<sub>2</sub>-MIL-101 (Al) has higher excess uptakes at higher pressures because of the different metal cluster interaction between Al and Cr with H<sub>2</sub>. Also, the -NH<sub>2</sub> group increases the weight of the framework, giving a lower gravimetric uptake as later shown for the IRMOF-1 and IRMOF-3 uptake differences. Figure 4 shows a UiO-67 excess isotherm with the same shape as in literature but with 20 % less uptake [42]. This difference has been attributed to sample variability. The synthesized UiO-67 batches show similar XRD patterns and lower BET surface areas from the N<sub>2</sub> isotherm data at 77 K ( $1347 \pm 55 \text{ m}^2 \text{ g}^{-1}$ , compared to  $1877 \text{ m}^2 \text{ g}^{-1}$  when using the same BET range, from 0.05 to 0.25 P/Po) that of literature.

All the characterization data obtained from literature and experimentation, including BET ranges used and detailed methodologies for each material can be found in the supplementary information document.

#### 4. Analysis and discussion

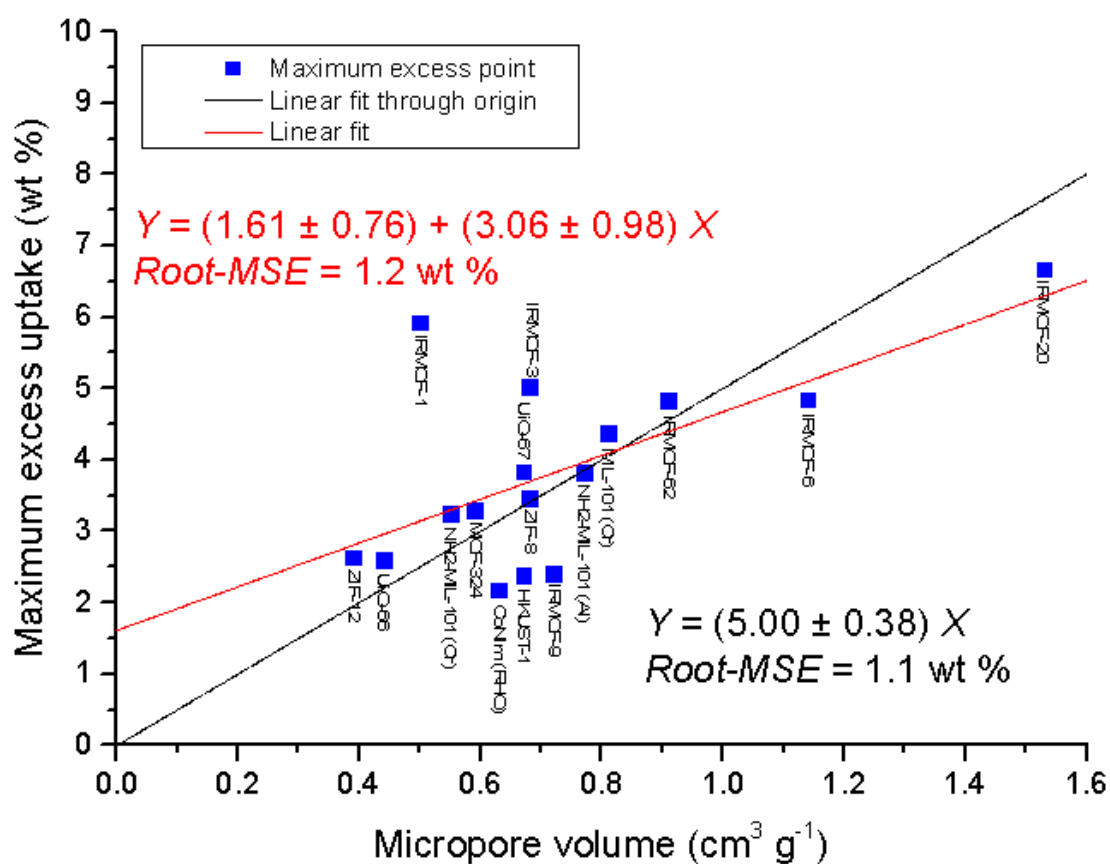
Comparing BET surface areas of MOFs with their uptakes at 0.1 MPa and 77 K proved the need to use higher pressures to compare their maximum excess uptakes instead, due to their different isotherm shapes [19]. As mentioned above, an approximate linear relationship was found when plotting the maximum excess uptake against their Langmuir surface area [20]. In Figure 5, the maximum hydrogen uptake of every MOF against the BET surface area divided by one thousand is plotted. Two linear fits were plotted, by fixing (black line) and not fixing the fit at the origin (red line), where  $x, y = 0$ . From the graph, it can be seen that high maximum excess corresponds to materials with high BET surface area, showing a linear relationship between the two variables with a certain degree of scattering. The red line fitting, (Root-MSE= 0.650 wt %) shows a slightly better fit than the black one (Root-MSE = 0.787 wt %) giving  $(1.05 \pm 0.33) + (1.35 \pm 0.14) x$  and  $(1.76 \pm 0.08) x$  wt % per  $1000 \text{ m}^2 \text{ g}^{-1}$  respectively. The correlation shows higher scattering at lower BET ranges, which it is believed to be related to their different pore volumes and smaller pore size. Also, it has been observed that the slope of the fit with fixed origin,  $1.76 \pm 0.08 \text{ wt \% per } 1000 \text{ m}^2 \text{ g}^{-1}$ , shows a very similar value that of the “Chahine rule”, with a value of  $2 \text{ wt \% per } 1000 \text{ m}^2 \text{ g}^{-1}$ . However, these values overestimate the value obtained from the best linear fit,  $1.35 \pm 0.14 \text{ wt \% per } 1000 \text{ m}^2 \text{ g}^{-1}$ . Both UiO-66 and 67 are above the linear correlation, outperforming compared to other family groups. This might indicate that a different topology might yield a higher uptake compared to other materials. Also, IRMOF-1 and IRMOF-3 show a very high uptake compared to their BET values. IRMOF-3 shows a slightly lower uptake than IRMOF-1, caused by differences in the functionalization of the linker. When calculating the differences between their molecular weights (no solvent) (in  $\text{g mol IRMOF}^{-1}$  [6, 12] and maximum molar uptakes (in  $\text{g H}_2 \text{ mol IRMOF}^{-1}$ ), values of 8.01 and 7.97 % were found respectively. This indicates that the amino group found in IRMOF-3 linkers increases the molecular weight of the framework, with the increase being inversely proportional to its hydrogen uptake. IRMOF-9 slightly underperforms compared to its surface area, even when possessing an interpenetrated structure. This adds extra weight in the structure together with the interpenetration itself that reduces the available pore volume, giving a lower uptake compared with other IRMOFs. ZIF-12 also shows higher uptake than expected compared to its surface area, probably due its small pore diameters (0.66 and 1.4 nm).



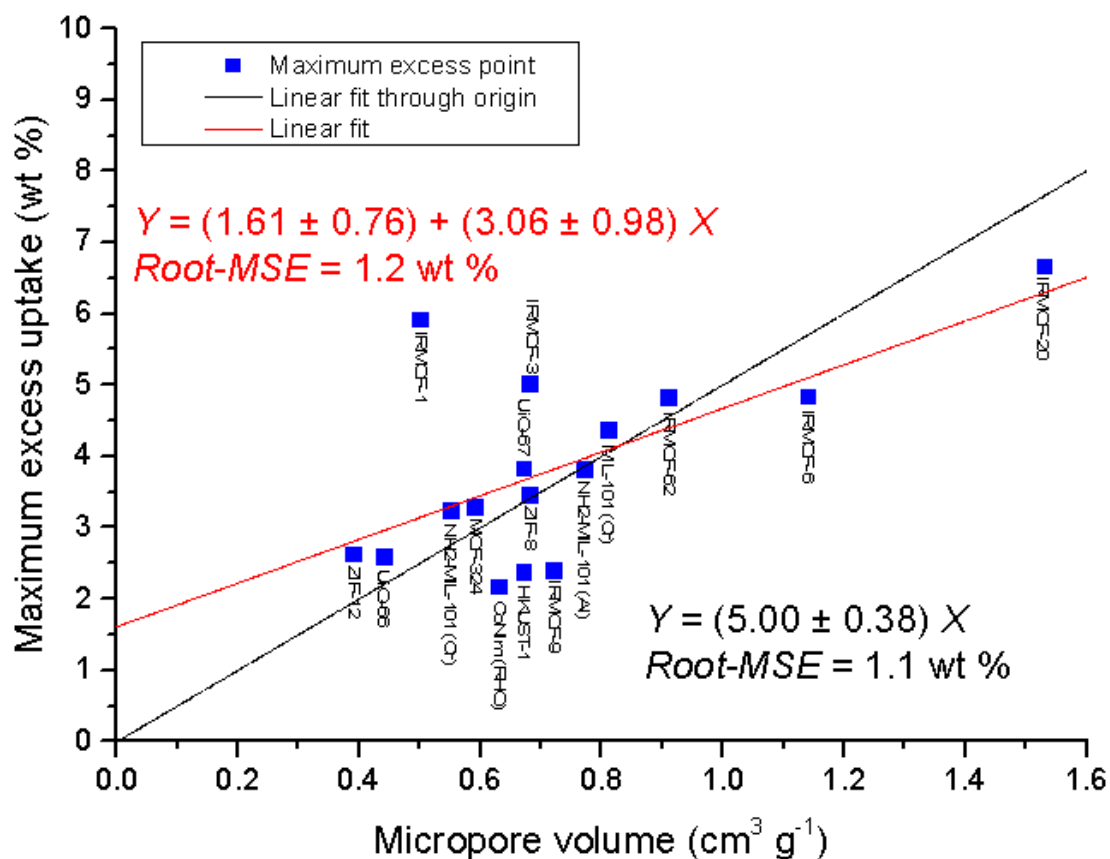
**Fig 5.** Maximum excess capacity of MOFs at 77 K vs BET surface area (N<sub>2</sub> at 77 K) in 1000 m<sup>2</sup> g<sup>-1</sup>. Error bars correspond to the standard deviation obtained from the BET calculation.

In Figure 6, all the available experimental and literature data with microporous volume using the DR methodology has been plotted against their maximum excess uptake. The graph shows a generalised increase in maximum excess uptake with increased microporous volume, existing a high degree of scattering, especially due to IRMOFs 1 and 3. The linear fittings show very low correlation values (Root-MSEs of 1.18 and 1.06 wt % respectively) giving  $(1.61 \pm 0.76) + (3.06 \pm 0.98) x$  and  $(5.00 \pm 0.38) x \text{ cm}^3 \text{ g}^{-1}$ . As in Figure 5, the value of the slope of the fit with fixed origin,  $5.00 \pm 0.38 \text{ wt } \% \text{ per micropore cm}^3 \text{ g}^{-1}$ , yields a very similar value that of the “Chahine rule”, with a value of 5 wt % per micropore cm<sup>3</sup> g<sup>-1</sup>. Again, this value overestimates the value obtained from the best linear fit  $3.06 \pm 0.98 \text{ wt } \% \text{ per micropore cm}^3 \text{ g}^{-1}$ . Previous publications also indicated the existence of scattered micropore volume relationships with activated carbons [15, 16, 19]. Also, it has been reported that the ideal pore size for maximal attraction of an adsorbate is the same as its kinetic diameter, stating the

influence of pore size for hydrogen adsorption [12]. Therefore, since in Figure 6, the micropore volume for each material is accounted for the same way, having different pore sizes and the rest of the pore volume (total pore volume minus micropore volume) is not considered, a high degree of scattering is observed. On top of that, the surface area, which shows a more linear relationship than the rest of the variables with hydrogen uptake, is higher in MOFs than other materials, such as activated carbons or zeolites, adding higher dispersion. Similar reasoning to explain the scattering can be used to describe Figure 7 since all pore volume is considered the same, neglecting any higher contribution from the micropores for each material (Root-MSEs of 0.99 and 1.35 wt % respectively).



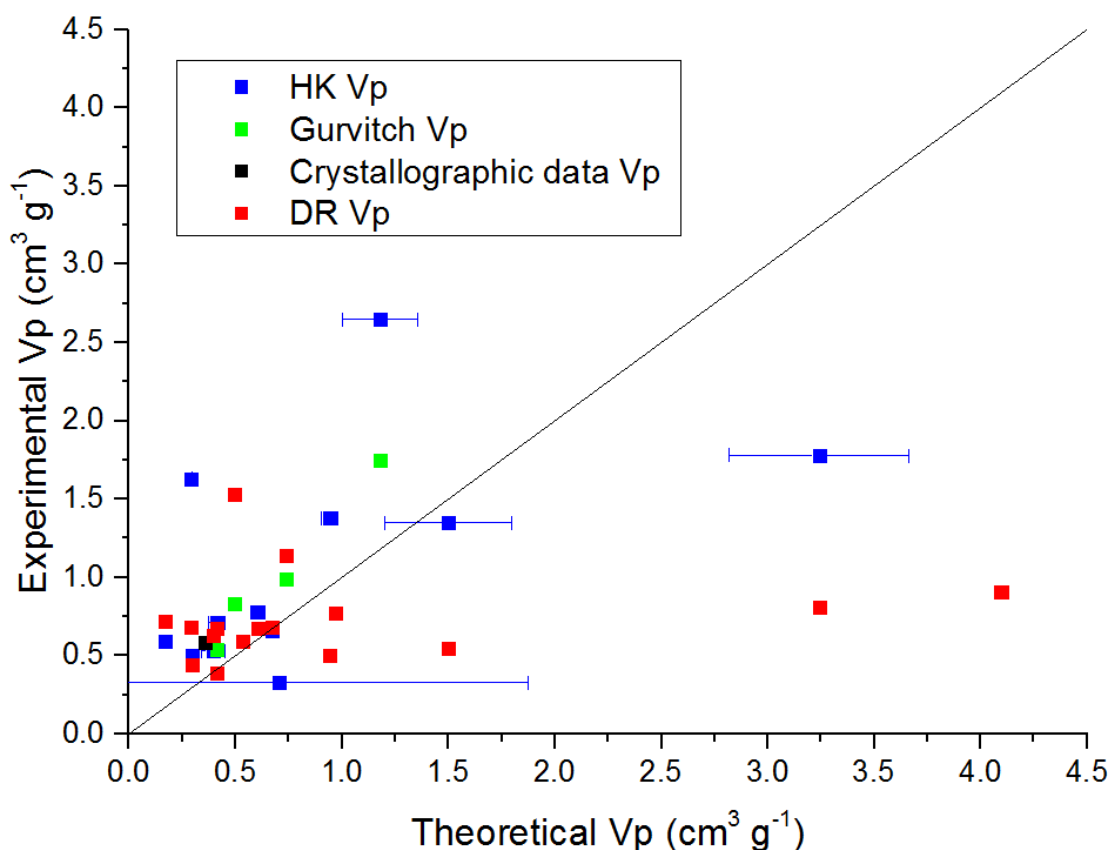
**Fig 6.** Maximum excess capacity of MOFs at 77 K vs microporous pore volume using the DR method.



**Fig 7.** Maximum excess capacity of MOFs at 77 K vs total pore volume (HK, Gurvitch, Single crystal and Cerius2 methodologies from experiments and literature used).

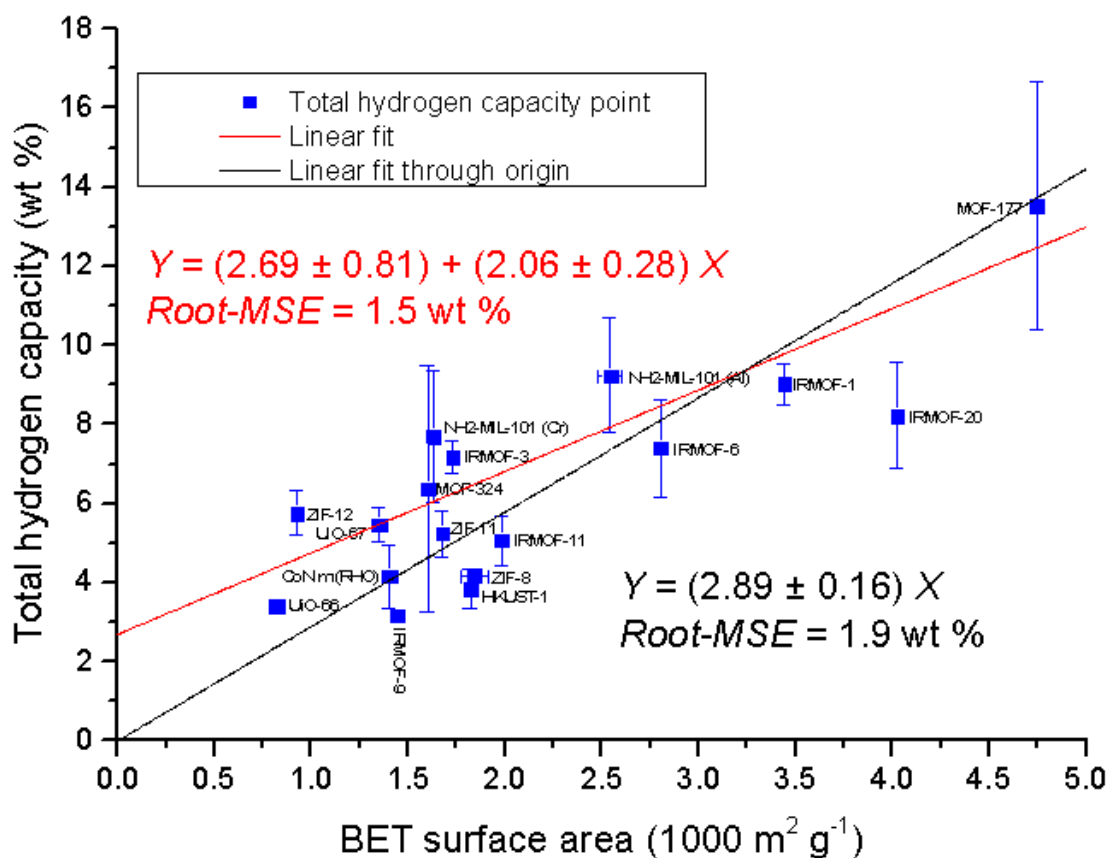
In Figure 8, the pore volume values obtained from the non-linear fitting in every fitted material are used, this being compared with all the pore values obtained from  $\text{N}_2$  sorption experiments and literature. A straight line with equation  $X = Y$  has also been plotted to help the reader see how close the pore volumes from the fitting compare to the experimental or literature ones. It can be seen that in many cases the fitted pore volume is relatively close to the experimental value obtained from different sources, especially at low pore volume values.





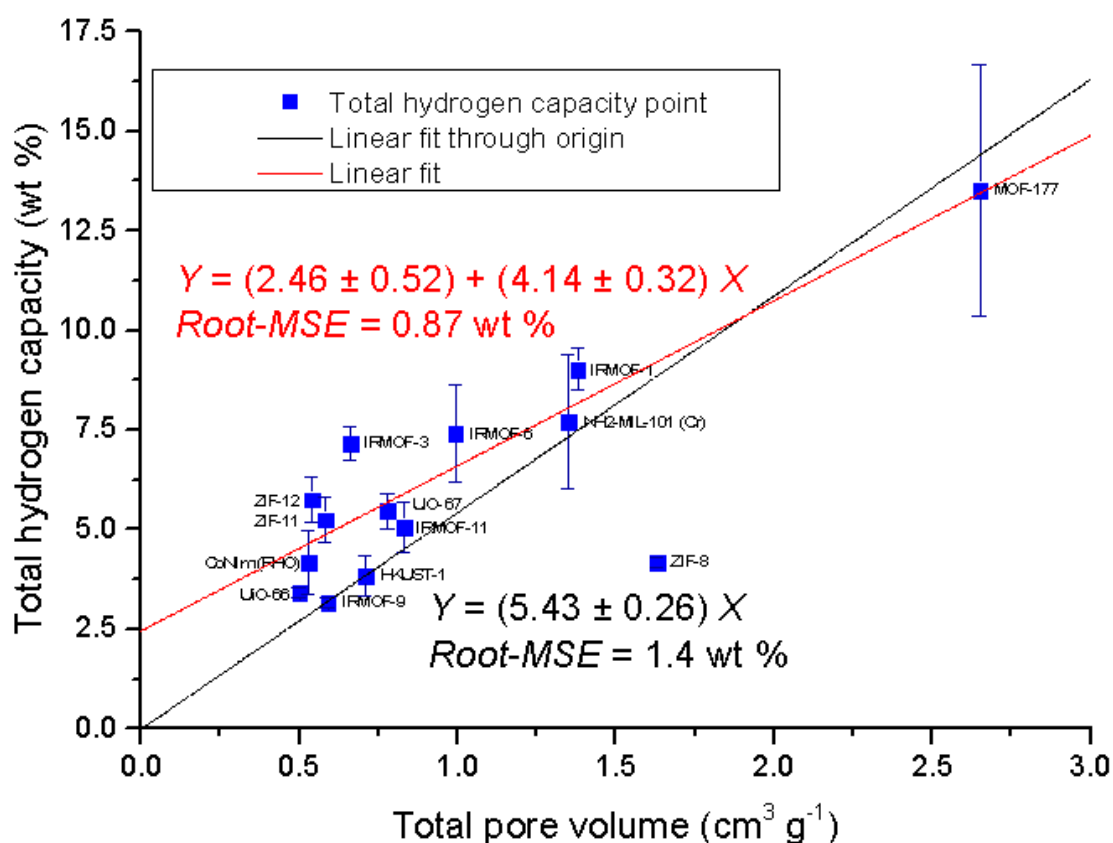
**Fig 8.** Theoretical pore volume obtained from fittings vs different experimental pore volumes. Error bars correspond to the standard error obtained from the model fitting.

Figure 9 shows BET surface area against the modelled total hydrogen capacity from model fitting, including error bars as the uncertainties from the calculation of the density of the adsorbate and pore volume obtained from the model fitting. Due to unrealistically high values from the fit and/or error bars, MIL-101 (Cr), MOF-74 and IRMOF-62 ( $19.25 \pm 2.65$ ,  $6.03 \pm 12.04$  and  $29.18 \pm 17.53$  wt % respectively) have not been used in the correlations. Although not as strongly correlated as when compared with the maximum excess uptake (Root-MSEs of 1.48 and 1.88 wt % respectively), a linear relationship between surface area and hydrogen capacity can be seen. From the linear fittings a relationship of  $(2.69 \pm 0.81) + (2.06 \pm 0.28) x$  and  $2.89 \pm 0.16$  total wt % per  $1000 \text{ m}^2 \text{ g}^{-1}$  respectively has been obtained. The correlation predicts that several materials will perform better than when compared with the excess uptake. Most of the materials that outperformed in previous correlations, do outperform here as well, showing also high potential for the MILs. This has been attributed to the MILs mesoporosity, which require higher pressures in order to reach pore saturation.



**Fig 9.** Total hydrogen capacity of MOFs vs BET surface area (N<sub>2</sub> at 77 K) in 1000 m g<sup>-1</sup>. Error bars correspond to the standard error of the product of  $\rho_A * V_p$  to yield total capacity.

In Figure 10, all available experimental and literature total pore volume methodologies (HK total pore volume, Gurvitch, Single Crystal XRD and Cerius2) has been plotted as a function of the total hydrogen capacity. With the exception of ZIF-8, all the materials show a linear although scattered relationship (Root-MSE values 0.87 and 1.41 wt % respectively), giving the fits  $(2.46 \pm 0.52) + (4.14 \pm 0.32) x$  and  $(5.43 \pm 0.26) x$  total wt % per cm<sup>3</sup> g<sup>-1</sup>. Reports in literature state lower total pore volume for ZIF-8 compared to the ones obtained experimentally, matching however, the BET surface area and microporous volume values [43]. The correlation gives slightly better results that when plotted against the maximum hydrogen excess for the linear fit that does not pass through the origin. This result is related to the model's assumption that all the materials' pores are filled with adsorbed hydrogen. Although it has been reported in literature that hydrogen is best adsorbed in micropores, at high pressures, the amount of hydrogen that can be adsorbed in the rest of the pores cannot be considered negligible.

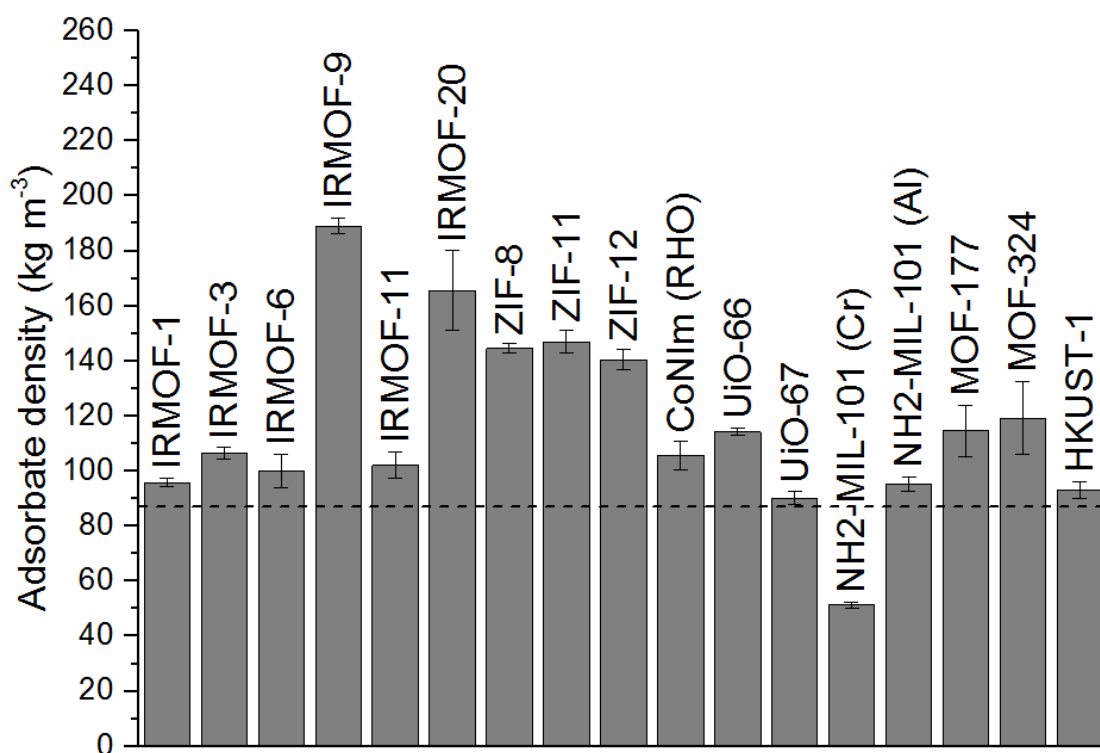


**Fig 10.** Total hydrogen capacity vs total pore volume (HK, Gurvitch, Single crystal and Cerius2 methodologies used). Error bars correspond to the standard error of the product of  $\rho_A * V_p$  to yield total capacity.

The microporous volume did not yield any correlation with the total hydrogen capacity. As previously discussed in Figure 6, many effects are not accounted for, these being even more significant since it is considering all the pores completely filled, giving the disregarded total pore volume even higher weighting. Pore size plots did not show any relationship either. This was because of the existence of different pore size ratios and microporous volumes in some materials as well as the DFT kernel limitations, allowing a limited amount of pore shapes that did not match MOFs topologies.

Figure 11 shows the predicted adsorbate density ( $\rho_A$ ) obtained from applying the model applied to each experimental hydrogen isotherm. Plotted error bars correspond to the uncertainty of the values obtained for the density of the adsorbate obtained from the fittings. Overall, it shows very high density values when compared with the density of solid hydrogen ( $87 \text{ kg m}^{-3}$  at 0 MPa and 4.4 K) [44]. IRMOF-9 shows the highest adsorbate density which can be related to its interpenetrated structure. However, an

interpenetrated structure that increases the density of the framework together with a low pore volume yields a low uptake and total hydrogen capacity. The second highest adsorbate density observed belongs to IRMOF-20, a material with a high surface area ( $4024 \text{ m}^2 \text{ g}^{-1}$ ) [45] and pore volume, with micropores (1.4 and 1.73 nm) [45-47]. Overall, most of the materials (IRMOF-1, IRMOF-3, IRMOF-6, ZIF-CoNIm, UiO-67,  $\text{NH}_2$ -MIL-101 (Al) and HKUST-1) show a hydrogen density around  $80\text{-}90 \text{ kg m}^{-3}$ . Since the total hydrogen capacity is calculated as the product of pore volume times the adsorbate density ( $V_p * \rho_A$ ), the total value can come from a high adsorbate density or a high  $V_p$  value that the model could have given.



**Fig 11.** Predicted adsorbate density of each MOF, including error bars from the model. Error bars come from the standard error of  $\rho_A$  when fitting the hydrogen isotherms to the model. Dashed line indicates the limiting density of solid hydrogen at 0 MPa ( $87 \text{ kg m}^{-3}$ ) [44].

## 5. Conclusions

Several MOFs have been tested at high pressures and 77 K for hydrogen adsorption and the pressure range at which some MOFs were tested in the past has been extended. ZIF-9 shows a similar behaviour to ZIF-7, which is known for having a sorbate-induced

gate-opening mechanism. Results indicate that ZIF-9 also has a gate-opening structure, indicating a possible relation between structural flexibility and SOD topology. However, no flexibility features were experimentally found in the gas sorption isotherms for ZIF-8. The uptakes of ZIF-7 and ZIF-9 are very similar to their RHO counterparts, ZIF-11 and ZIF-12. This indicates little or no effect on hydrogen excess adsorption when the ZIF has Zn or Co as part of the metal cluster. Also, the relationship between the uptake of the SOD and RHO topologies indicates the RHO topology to be a favourable topology because of the far greater uptake shown compared to the SOD topology for the tested ZIFs. This also indicates the existence of a hydrogen uptake correlation with topology.

The existence of a linear relationship between maximum hydrogen uptake and MOFs for both surface area and microporous volume have been shown, as in other studies with different adsorbents [15-19]. Also, the correlations with the modelled total pore volume have shown correlations with surface area and total pore volume, the latter having slightly lower Root-MSE when compared with the maximum hydrogen uptake correlation for the non-fixed linear fit. This is likely to be because the model considers all the materials' pores fully filled with adsorbed hydrogen, accounting for the total pore volume filled to its maximum capacity. Possible pore size relationships were also checked, not yielding any correlation probably due the mix of different pore sizes for many of the chosen materials.

From the linear fittings applied to each correlation, it has been observed that the two parameter linear fitting always gave lower Root-MSE values in all cases. This leads to linear correlations with both maximum hydrogen uptake and total hydrogen capacity, unlike the correlations seen in previous studies, which always pass through the origin. However, as no previous work related to this topic state any statistical quantity to state the goodness of the correlations, more detailed comparisons cannot be made.

When the maximum excess uptake correlations fitted through the origin are compared with the "Chahine rule", many similarities can be seen. From the surface area correlations  $1.76 \pm 0.08$  wt % per  $1000 \text{ m}^2 \text{ g}^{-1}$  was obtained from this work compared to 2 wt % per  $1000 \text{ m}^2 \text{ g}^{-1}$  from the "Chahine rule". Also, from the microporous pore volume correlations  $5.00 \pm 0.37$  wt % per  $\text{cm}^3 \text{ g}^{-1}$  of micropore volume was obtained

from this work compared to 5 wt % per  $\text{cm}^3 \text{g}^{-1}$  of micropore volume. However, the two parameter linear fittings gave lower Root-MSE values, indicating that the “Chahine rule” overestimates the maximum hydrogen uptake predictions.

Nevertheless, these correlations still only predict the increasing hydrogen uptake with increasing surface area and pore volume, and does not allow prediction of the minimum necessary intrinsic properties needed. By contrast, the novel correlations with the modelled total hydrogen capacity presented here can provide more practical predictions, enabling the calculation of a specific amount of hydrogen contained in a tank from the surface area and pore volume of a given MOF.

Regarding these total hydrogen capacity correlations, two new equations for surface area and total pore volume were obtained  $((2.69 \pm 0.81) + (2.06 \pm 0.28)$  total wt % per  $1000 \text{ m}^2 \text{ g}^{-1}$  and  $(2.46 \pm 0.52) + (4.14 \pm 0.32)$  total wt % per  $\text{cm}^3 \text{ g}^{-1}$  of total pore volume. However, the model showed higher hydrogen adsorbate density within the pores of most of the materials compared to solid hydrogen ( $87 \text{ kg m}^{-3}$  at 0 MPa and 4.4 K) [44]. Therefore these equations, in conjunction with system masses and volumes, would help predict the properties a MOF would need to have in order to meet the US DOE targets, to allow hydrogen to be used as an energy vector for sustainable applications such as light-duty transport vehicles. A high surface area and a high pore volume are of utmost importance for the design of high hydrogen capacity nanoporous materials. Also, from literature, a narrow pore size distribution of around 0.7 nm has been proved to be of paramount importance for a more optimal storage of hydrogen, and according to results shown here, some topologies that have pore sizes in that range seem to perform better for total hydrogen uptake [18]. The materials with UiO topology (Zr), UiO-66 and UiO-67 outperformed most of the fittings through the origin in the correlations. This has mainly been related to their small pore sizes and topology (0.75 and 1.2 nm for UiO-66 and 1.2 and 1.6 nm for UiO-67), these being close to the stated optimum for hydrogen storage, 0.7 nm [18, 48]. However, UiO-67 pore size is over 35 % larger compared to the optimum. HKUST-1, despite its reasonable surface area ( $1343 \pm 82$ ), micropore volume ( $0.67 \text{ cm}^3 \text{ g}^{-1}$ ) and very small pore sizes (0.46 and 0.85 nm, DFT slit  $\text{N}_2$ ) shows a lower than predicted hydrogen uptake, being under the fixed linear fitting in most of the correlations.

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