

Performance optimisation of room temperature magnetic refrigerator with layered/multi-material microchannel regenerators

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Abstract

A hybrid numerical model of the magnetic refrigerator with multi-material microchannel regenerator has been developed. The magnetocaloric effect was implemented using instantaneous temperature rise/drop (discrete method). Two pipe-in-pipe heat exchangers at two ends of the regenerator were treated using ϵ -NTU method. The commercially available compounds of $\text{LaFe}_{13-x-y}\text{Co}_x\text{Si}_y$ as well as hypothetical compounds of Gadolinium were considered as the magnetocaloric materials (MCMs) with different Curie temperatures. The predicted results of the present work for parallel regenerators employing different compounds of $\text{LaFe}_{13-x-y}\text{Co}_x\text{Si}_y$ were broadly in good agreement with the available experimental data. The cooling capacity increases as the number of MCMs increase. However, for a given length of regenerator, an optimum number of MCMs was seen yielding the maximum performance of the refrigerator. For a given number of MCMs, a smaller Curie temperature difference ΔT_{Cu} between the MCMs was found to give higher performance.

Key words: Magnetic refrigeration, Microchannel regenerator, Numerical modelling, Magnetocaloric material, Multi-material/Layered regenerator

Highlights:

- A multi-MCM microchannel regenerator is used for numerical simulation of magnetic refrigerators.
- 25% higher no-load temperature span was achieved with 3-MCMs compared to single MCM.
- Optimised Curie temperatures difference of two consecutive MCMs is found in a given range.
- Influence of hot end temperature on the cooling capacity is investigated.

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1. Introduction

Magnetocaloric effect (MCE) is a phenomenon exhibited by certain rare earth metals such as Gd, Mn, Yd, La and their alloys etc. in the form of temperature or entropy change upon their exposure to a changing magnetic field. The materials exhibiting MCE are known as the magnetocaloric materials (MCMs). The severity/magnitude of MCE is strongly reliant upon of the change in the magnetic field (ΔB) as well as the temperature of the MCM [1, 2]. The peak MCE is observed when the temperature of the MCM is the same as Curie temperature of the MCM and its value drops as the temperature of the MCM differs from its Curie temperature. **Figure 1** shows the dependence of MCE on the temperature of the MCM and change in magnetic field for different MCMs [3]. Gadolinium (Gd) has Curie temperature of 24° C and it shows the maximum temperature change per unit change in the magnetic field among the second order magnetic transition (SOMT) materials (up to 3.0 KT^{-1} theoretical value and 1.5-2.0 KT^{-1} experimental [4]). It has thus become the most commonly employed MCM in magnetic refrigeration till date [5-7].

Magnetic refrigeration is a promising new technology with potential to provide an alternative for conventional refrigeration techniques. It employs the phenomenon of MCE to produce useful cooling/heating. There are three different cycles upon which a magnetic refrigerator can be operated (a) Magnetic Carnot Cycle; (b) Magnetic Ericsson Cycle and (c) Magnetic Brayton or Active Magnetic Regenerative Cycle. The Carnot cycle serves as a theoretical reference for the performance comparison of other operating cycles. The Ericsson cycle requires very large magnetic field change to produce significant cooling and temperature span. Electromagnets are normally used to produce magnetic fields larger than 1.5 T but their operation can be cumbersome and expensive when compared with a permanent magnet assembly [8]. A significant number of prototype magnetic refrigerators have been developed over the last two decades operating on active magnetic regenerative cycle [5-7]. Active magnetic regeneration is based on progressively building a temperature gradient along the length of the MCM regenerator. The cycle consists of four stages namely (i) magnetisation; (ii) flow from one end to other through the MCM; (iii) demagnetisation; (iv) flow from reverse end. As the number of regenerative cycles increase the temperature at one

end is maintained at the ambient temperature while at the other end temperature continues to drop (to form the cold end) till a steady state longitudinal/axial temperature gradient is established. The difference of temperature at ends is temperature span of the magnetic refrigerator for a given cooling load. Single MCM, such as Gd based regenerators show limited temperature spans across two ends of the regenerator [6]. One of the factors restricting the temperature span is the gradual decline in MCE value since the local temperature of the MCM has commenced to deviate from its Curie temperature. During subsequent magnetisations/demagnetisations, the MCM regions possessing temperature closer to its Curie temperature experience relatively larger MCE whereas the regions with temperature farther from the Curie value undergo smaller MCE. This behaviour ultimately limits the maximum achievable temperature span across the regenerator. One common method of enlarging the regenerator temperature span is by the use of more than one MCM with different Curie temperatures along the length of regenerator [9-16]. MCM with the lowest T_{Cu} is laid at the cold end while the MCM with highest T_{Cu} at the hot end so that each MCM experiences maximum possible MCE. Arnold et al.[9] conducted experiments on two-MCM based regenerators under 2 T and 5 T. No-load temperature spans of 33 K and 59 K were reported under 2 T and 5 T, respectively. Tusek et al. [10] performed experimental investigations on four different compound of LaFeCoSi having tailored Curie temperatures. Similarly, Legait et al. [11] employed three different types of MCMs with tailored Curie temperatures in different regenerators and reported larger temperature span for the multi-MCM regenerator. Aprea et al.[12] employed three MCMs to examine the performance of a layered regenerator. However, the chosen MCMs were not possessing specifically tailored (Gd: $T_{Cu} = 294$ K; Dy: $T_{Cu} = 179$ K; Tb: $T_{Cu} = 230$ K) and thus resulted in insignificant improvement in the performance. Hsieh et al. [13], Monfared and Palm [14] and Lie et al. [15] numerically evaluated the performance of layered bed regenerator using Gd_xTb_{1-x} alloys and inferred that two and three MCM based regenerators yielded considerably better performance compared to single material regenerator.

Importantly, recent research in magnetocaloric materials (Katter et al. [17], Katter et al. [18], Katter et al. [19], Bjork et al. [20], Barcza et al. [21], Bahl et al. [22], Radulov et al. [23] and Pulko et al.[24]) demonstrates the possibility of tailoring the Curie temperature of alloy MCMs to desired values (in the room temperature range) by changing the chemical composition of its constituting elements. Katter et al. [19] and Bjork et al. [20] have reported the tuning of magnetocaloric characteristics of $\text{LaFe}_{13-x-y}\text{Co}_x\text{Si}_y$ compounds. The Curie temperatures of these compounds were altered by varying the percentage mass of their chemical constituents La, Fe, Co and Si. Various compounds of $\text{LaFe}_{13-x-y}\text{Co}_x\text{Si}_y$ have been prepared with different Curie temperatures and are available commercially (e.g. Vacuumschmelze GmbH).

Experimental comparisons performed by Tusek et al. [10] and Legait et al. [11] between single and multi-MCM regenerator reveal improved performance of magnetic refrigerator while using multi-MCM regenerator. However, experimental investigations are constrained by number of possible multi-MCM settings that can be examined such as number of MCMs, Curie temperature of the MCMs and Curie temperature difference between two adjacent materials. In addition, due to unavailability of Gd based alloys, the majority of comparisons have been made for non-Gd MCMs and their respective alloys. So far single-MCM Gd regenerator has been reported to show larger temperature span compared to multi-MCM non-Gd regenerator [10, 11]. It can thus be expected that a multi-MCM regenerator with different Gd alloys would yield considerably better performance than the multi-MCM regenerator of non-Gd alloys such as $\text{LaFe}_{13-x-y}\text{Co}_x\text{Si}_y$. The present work numerically evaluates the performance of a multi-MCM microchannel regenerator employing hypothetical compounds of Gd. The present numerical predictions can pave the way for future developments of Gd based alloys/compound and their applications in active magnetic regenerator.

Single Column Figure

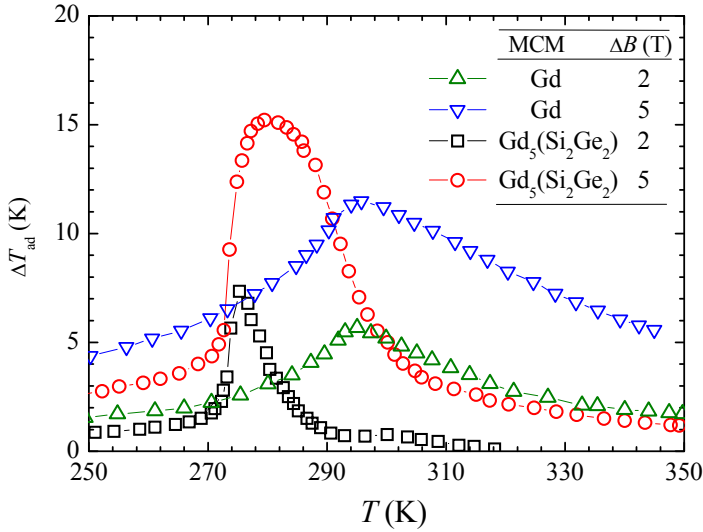


Figure 1 Variation of adiabatic temperature change ΔT_{ad} with temperature for different magnetic field variations (reproduced from Pecharsky and Gschneidner Jr. [3]).

2. Physical model of magnetic refrigerator

The operating cycle of the magnetic refrigerator is simulated to predict and optimise the performance. The five main components of the magnetic refrigerator i.e. regenerator, permanent magnet assembly (magnetic field source), heat exchangers and displacer are modelled as shown in **Figure 2**. The schematic of fluid flow and heat transfer through one channel of the multi-MCM regenerator are shown in **Figure 3**. The magnetization and demagnetization occur in the regenerator when there is a relative motion between the magnet and regenerator. The temperature of the MCM rises during magnetisation while it drops during demagnetisation. The fluid flow occurs in between magnetisation and demagnetisation. The CHEX and HHEX are concentric tube heat exchangers. Water is used as the working fluid.

To simplify, the following assumptions and approximations are made:

- 1) Magnetic field is uniform in the regenerator and the demagnetizing field is neglected;
- 2) Thermal and magnetic hystereses of MCM are negligible;
- 3) Properties of the MCM are independent of temperature and magnetic field intensity;
- 4) Flow is incompressible;
- 5) Thermophysical properties of the working fluid are taken to be constant;
- 6) Viscous dissipation is neglected;

- 7) Heat loss to the ambient is neglected;
- 8) There are no fluid leakages in loops;
- 9) The dead volume of fluid inside the entire system is zero.

1.5 Column Figure

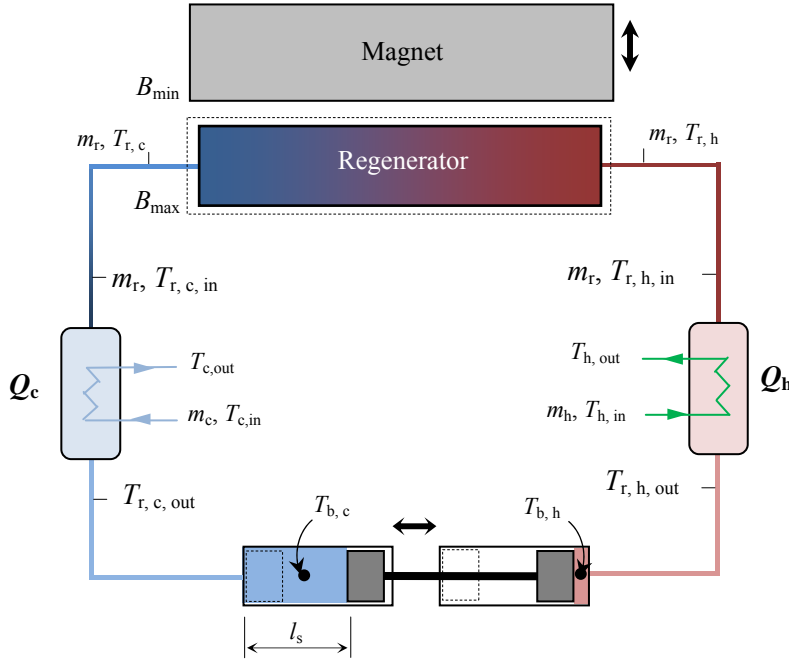


Figure 2 Simulation model of the magnetic refrigerator

3. Mathematical model

In this section, the mathematical models for the conjugated transfer in regenerator, magnetic field source (MCE), heat transfer in the heat exchangers and fluid displacer are presented.

3.1 Regenerator

Figure 3(a) shows the schematic of a multi-MCM microchannel regenerator which has the width W , height H and length L . The regenerator is split along its length into n number of sections of equal length L/n as shown in **Figure 3(b)**. Each section corresponds to a separate MCM with different Curie temperature. Considering symmetry, conjugated conductive heat transfer in the MCM wall and convective heat transfer in one channel are simulated. The x -coordinate is taken at the centre of the channel from the cold end. A photograph of the manufactured microchannel regenerator made of Gd is presented in **Figure 4**.

Double Column Figure

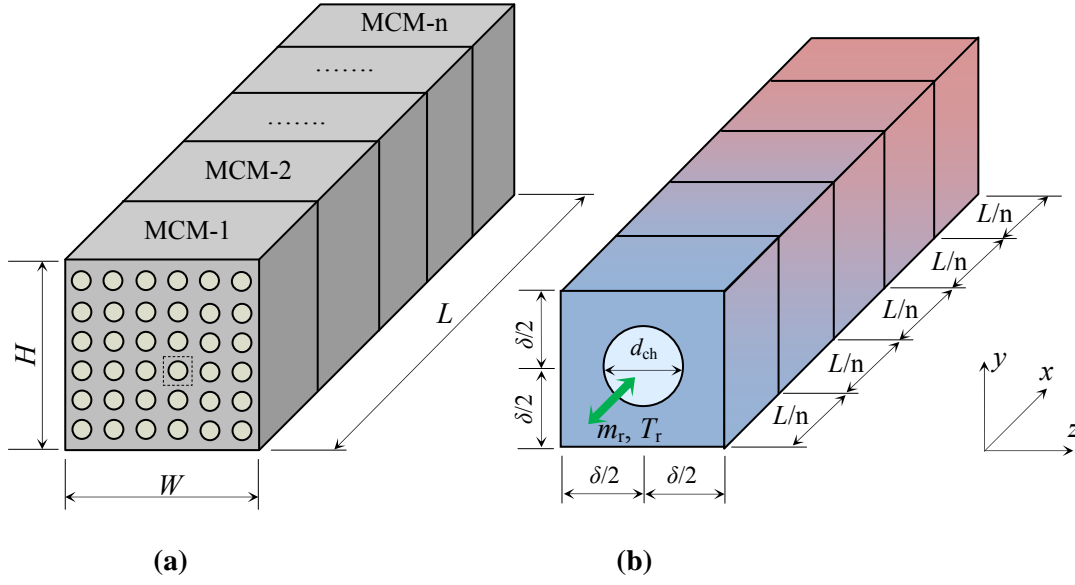


Figure 3 (a) Schematic of the multi-MCM microchannel regenerator; (b) Schematic of one channel simulated in this work.

Single Column Figure

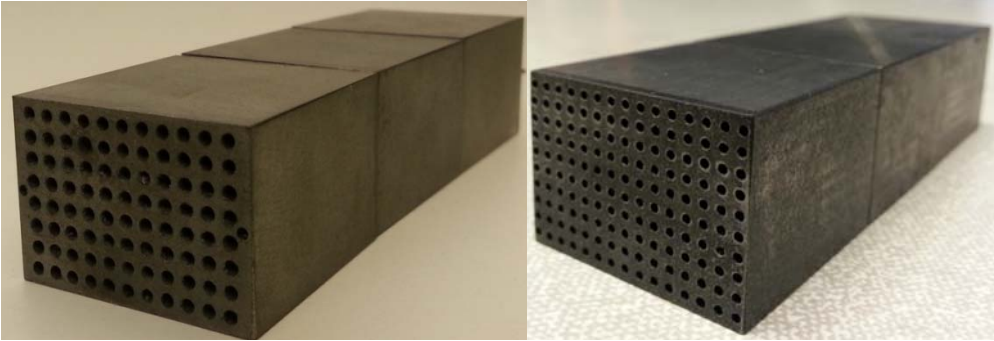


Figure 4 A photograph of the manufactured microchannel regenerator

The conservations of mass, momentum and energy are written as:

$$\nabla \cdot \mathbf{u} = 0 \quad (1)$$

$$\rho_f \left(\frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} \right) = -\nabla P + \mu_f (\nabla^2 \mathbf{u}) \quad (2)$$

$$\frac{\partial T_f}{\partial t} + \mathbf{u} \cdot \nabla T_f = \alpha_f (\nabla^2 T_f) \quad (3)$$

$$\frac{\partial T_s}{\partial t} = \alpha_s (\nabla^2 T_s) \quad (4)$$

where \mathbf{u} is the velocity of water, t is time, T_f and T_s are temperatures of water and MCM solid, respectively, ρ_f , μ_f and α_f are the density, dynamic viscosity and diffusivity of water, respectively, and α_s is the diffusivity of the MCM solid.

The boundary conditions are:

$$q = 0, u = v = w = 0 \quad \text{at} \quad x = 0, x = L \quad \text{and} \quad y^2 + z^2 - d^2/4 > 0 \quad (5)$$

$$\lambda_f \left(\frac{\partial T_f}{\partial \mathbf{n}} \right) = \lambda_s \left(\frac{\partial T_s}{\partial \mathbf{n}} \right) \quad \text{at} \quad 0 \leq x \leq L, y^2 + z^2 - d^2/4 = 0 \quad (6)$$

$$\frac{\partial T_s}{\partial \mathbf{n}} = 0 \quad \text{at} \quad 0 \leq x \leq L, y = \delta/2, -\delta/2 < z < \delta/2 \quad (7)$$

$$\frac{\partial T_s}{\partial \mathbf{n}} = 0 \quad \text{at} \quad 0 \leq x \leq L, -\delta/2 < y < \delta/2, z = \delta/2 \quad (8)$$

Cold blow (for $t = t_3 - t_4$, see **Figure 5**)

$$u_{r,c} = \frac{m_r}{\rho_f A_{ch} n_{ch}}, T_{r,c} = T_{r,c,in} \quad \text{at} \quad x = 0, y^2 + z^2 - d^2/4 < 0 \quad (9)$$

$$\frac{\partial \mathbf{u}}{\partial \mathbf{n}} = 0, \frac{\partial T_f}{\partial \mathbf{n}} = 0 \quad \text{at} \quad x = L, y^2 + z^2 - d^2/4 < 0 \quad (10)$$

Hot blow (for $t = t_6 - t_7$, see **Figure 5**)

$$u_{r,h} = \frac{m_r}{\rho_f A_{ch} n_{ch}}, T_{r,h} = T_{r,h,in} \quad \text{at} \quad x = L, y^2 + z^2 - d^2/4 < 0 \quad (11)$$

$$\frac{\partial \mathbf{u}}{\partial \mathbf{n}} = 0, \frac{\partial T_f}{\partial \mathbf{n}} = 0 \quad \text{at} \quad x = 0, y^2 + z^2 - d^2/4 < 0 \quad (12)$$

The MCE is implemented using the *discrete method* [25]. During the processes of magnetization and demagnetization, local temperature at the time t^{n+1} ($t^{n+1} = t^n + \Delta t$) takes a value at the time t^n with an instantaneous temperature *jump* calculated by Eq. (13).

$$T_s(x, y, z, t^{n+1}) = T_s(x, y, z, t^n) \pm \Delta T_{ad} \left[T_s(x, y, z, t^n), \Delta B \right] \quad (13)$$

where $T_s(x, y, z, t^{n+1})$ and $T_s(x, y, z, t^n)$ represent temperatures in solid MCM at location (x, y, z) and times t^{n+1} and t^n , respectively, ΔT_{ad} is positive during magnetization and negative during demagnetization. The adiabatic temperature change is determined by Eq. (14) [1].

$$\Delta T_{\text{ad}}(B, T_s) = - \int_{B_{\text{min}}}^{B_{\text{max}}} \frac{T_s}{c_{p,s}(B, T_s)} \frac{\partial m}{\partial T} dB \quad (14)$$

where $c_{p,s}(B, T)$ is the heat capacity of the MCM, and is the sum of the lattice $c_{\text{lat}}(T)$, electronic $c_{\text{ele}}(T)$ and magnetic $c_{\text{mag}}(B, T)$ heat capacities as given below:

The calculation of the MCE using the mean field model [17, 20] involves iterative solution for a set of non-linear equations and it can be computationally expensive for a 3D computational domain. To expedite the computation of the dynamic heat pump/refrigerator system, polynomial fit was applied to correlate ΔT_{ad} and T_s . For a given magnetic field intensity, ΔT_{ad} is solely a function of local temperature T_s of the solid. Two polynomials (Eqs. (15) and (16)) were found for temperatures lower and higher the Curie temperature ($T_{\text{Cu}} = 294.0$ K). Equations (15) and (16) are used in the present simulation.

$$\Delta T_{\text{ad}}(T_s, \Delta B = 1.0\text{T}) = a_1 T_s^3 + a_2 T_s^2 + a_3 T_s + a_4 \quad \text{for } T_s \leq T_{\text{Cu}} \quad (15)$$

$$\Delta T_{\text{ad}}(T_s, \Delta B = 1.0\text{T}) = b_1 T_s^3 + b_2 T_s^2 + b_3 T_s + b_4 \quad \text{for } T_s > T_{\text{Cu}} \quad (16)$$

Figure 5(a) shows the variation of ΔT_{ad} with temperature for Gd ($T_{\text{Cu}} = 294$ K) and two hypothetical materials with Curie temperatures at 289 K and 284 K, respectively. Use of three MCM regenerator would be able to provide a temperature jump of ~ 3 K over a temperature range of ~ 15 K while for single material this range is limited to just ~ 5 K.

Various ΔT_{ad} profiles for different MCMs are shown in **Figure 5(b)**. The ΔT_{ad} curves for different hypothetical materials are obtained by shifting the curve peak of ΔT_{ad} profile of Gd from 294.0 K to desired temperatures for $\Delta B = 1.0$ T. Polynomial fit was applied to correlate ΔT_{ad} and T_s and two polynomials are obtained for each MCM. Similar polynomial fittings have also been

applied for different ΔT_{ad} vs T_s curves plotted in **Figure 5(b)** and the polynomial coefficients of each material are listed in **Table 1**.

Single Column Figure

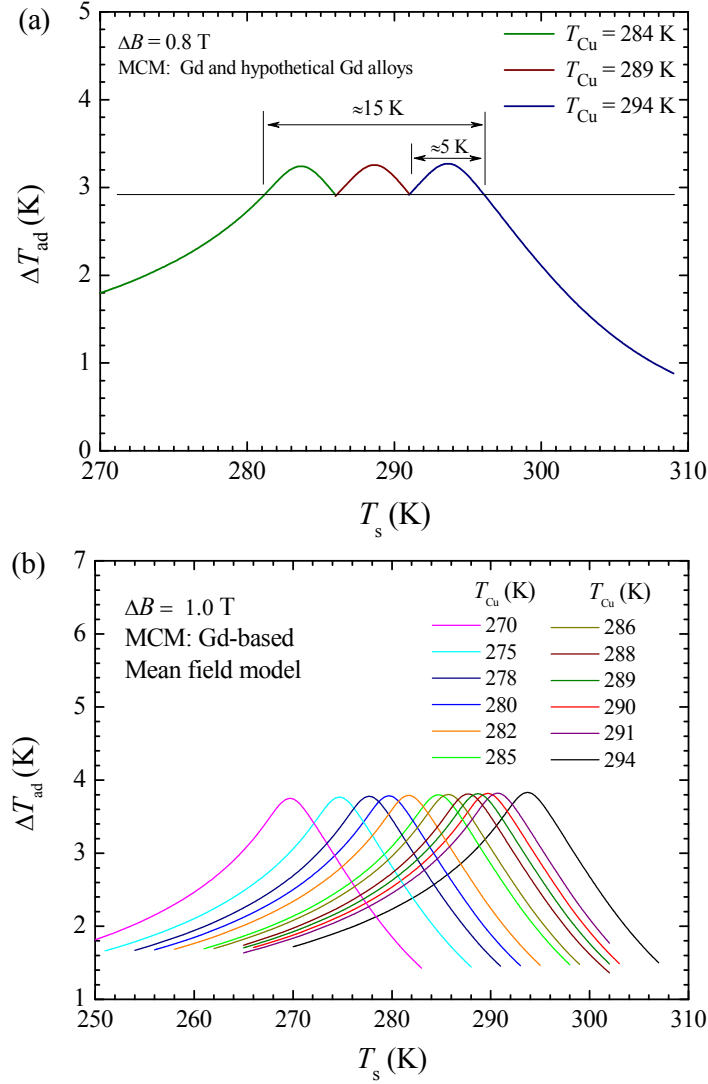


Figure 5 Variation of ΔT_{ad} with temperature for different values of ΔB and Curie temperatures predicted by mean field model (Morrish).

Table 1 Coefficients in Eqs. (15) and (16) for different Curie temperatures and magnetic field intensity $\Delta B = 1.0$ T.

T_{Cu} K	Polynomial coefficients							
	$T_s \leq T_{\text{Cu}}$				$T_s > T_{\text{Cu}}$			
	a_1	a_2	a_3	a_4	b_1	b_2	b_3	b_4
270	7.802838×10^{-5}	-5.721281×10^{-2}	14.020955	-1.146817×10^3	-5.395199×10^{-5}	5.020467×10^{-2}	-15.574492	1.611033×10^3
275	7.722034×10^{-5}	-5.775379×10^{-2}	14.435696	-1.204251×10^3	-5.283248×10^{-5}	5.002822×10^{-2}	-15.791982	1.662083×10^3
280	7.641005×10^{-5}	-5.826873×10^{-2}	14.848947	-1.262897×10^3	-5.173429×10^{-5}	0.983648×10^{-2}	-16.002893	1.713240×10^3
285	7.565805×10^{-5}	-5.880683×10^{-2}	15.273674	-1.323920×10^3	-5.056740×10^{-5}	4.955020×10^{-2}	-16.183475	1.762122×10^3
290	7.486439×10^{-5}	-5.928784×10^{-2}	15.688048	1.385368×10^3	-4.952326×10^{-5}	4.934121×10^{-2}	-16.384612	1.813737×10^3
282	7.609028×10^{-5}	-5.847142×10^{-2}	15.014828	1.286783×10^3	-5.121935×10^{-5}	4.968313×10^{-2}	-16.063928	1.731606×10^3

3.2 Heat exchangers

The heat exchangers at the cold and hot ends of the regenerator have been simulated using ε - NTU method [26]. The flow arrangement in the heat exchangers is set to be counter-current when fluid enters the heat exchanger from the regenerator side and becomes parallel when the flow direction is reversed. The heat transfer rates at the HHEX and CHEX, the heating and cooling loads, can be calculated by Eq. (17).

$$Q_j = \frac{1}{\tau} \int_0^{\tau} m_j c_{p,j} (T_{j,out} - T_{j,in}) dt \quad (17)$$

where m_j is the mass flow rate, $T_{j,out}$ and $T_{j,in}$ are the temperatures at the outlet and inlet, respectively, $c_{p,j}$ is the specific heat capacity of the fluid, τ is the period of a cycle. Here subscript j refers to hot or cold i.e. h or c. The temperature at the inlet of the heat exchanger $T_{j,in}$ is determined from numerical solution at the exit of the regenerator, while the temperature at the outlet $T_{j,out}$ is calculated using ε - NTU method (Cengel [27]).

For $Re < 2300$, Gnielinski [28] correlation is used,

$$Nu = \frac{(f_D / 8)(Re - 1000)Pr}{1 + 12.7\sqrt{f_D / 8}(Pr^{2/3} - 1)} \quad (18)$$

where f is the Darcy friction factor calculated by the Filonenko [29] correlation.

$$f_D = (1.58 \ln Re - 3.28)^{-2} \quad (19)$$

Equation (18) is valid in the ranges of $Re = 2300 \sim 10^6$, $Pr = 0.6 \sim 10^5$.

For laminar flow ($Re < 2300$),

$$Nu = 3.66 \quad (20)$$

$$f_D = 64 / Re \quad (21)$$

3.3 Displacer

Due to the horizontal reciprocating motion of the piston, the mass flow rate of the working fluid is determined by

$$m_r = \frac{1}{2} \pi \rho_f d_p^2 R f \sin(2\pi ft) \quad (22)$$

where R is the radius of the crank disk of the displacer ($l_s = 2R$), f is the rotational frequency of the crank disk and d_p is the cross-sectional diameter of the cylinder.

The average mass flow rate during the cold or hot blows is determined as

$$m_{r,av} = \frac{1}{\tau_{flow}} \int_0^{\tau_{flow}} m_r(t) dt \quad (23)$$

Assuming instant mixing of the fluid inside the chamber, the enthalpy-averaged bulk temperature $T_{b,j}$ of the fluid inside the chamber is calculated by

$$T_{b,j} = \frac{\int_0^{\tau_{flow}} m_r(t) T_{r,j,out} dt}{\int_0^{\tau_{flow}} m_r(t) dt} \quad (24)$$

Utilization, which is the ratio of thermal mass of fluid to thermal of solid, can be defined as

$$\varphi = \frac{m_{r,av} c_{p,f} \tau_f}{m_s c_{p,s}} \quad (25)$$

where τ_f is the time period for cold/hot blow and m_s is the mass of the magnetocaloric material.

3.4 Computation scheme

The procedure starts by creating 3D geometry and grid for the regenerator and defining the operating parameters such as the magnetic field intensity, the cycle frequency (hot and cold blow durations, magnetisation and demagnetisation durations) and the mass flow rate. The initial temperature (at $t = 0$ s) of the regenerator solid and the fluid inside the entire system is taken to be 293.0 K. The mass flow rate and magnetic field profiles are shown in **Figure 6**. The grid independence of the numerical results was achieved by varying the number of divisions along x , y and z directions for single blow steady state conjugated heat transfer in a channel. A summary is presented in **Table 2**. The width, height and length of the solid having a microchannel of diameter d_{ch} (see **Figure 3(b)**) are considered to be δ_x , δ_y and L , respectively. The number of divisions along x , y and z directions are represented by $n_{\Delta x}$, $n_{\Delta y}$ and $n_{\Delta z}$, respectively. The total number of control volumes are given by n_{CV} . The average Nusselt number was calculated for different mesh sizes. The mesh with $10 \times 10 \times 90$ divisions was selected for the present numerical simulation.

Equations (1) to (4) together with boundary conditions (Eqs. (5) - (12)) were numerically solved using Fluent. The SIMPLE algorithm was chosen. The simulations of the regenerator, calculations of CHEX and HHEX, mass flow rate of the working fluid by the displacer as well as the MCE caused by the magnetic field source were all coupled together with the help of user defined functions (UDF).

Single Column Figure

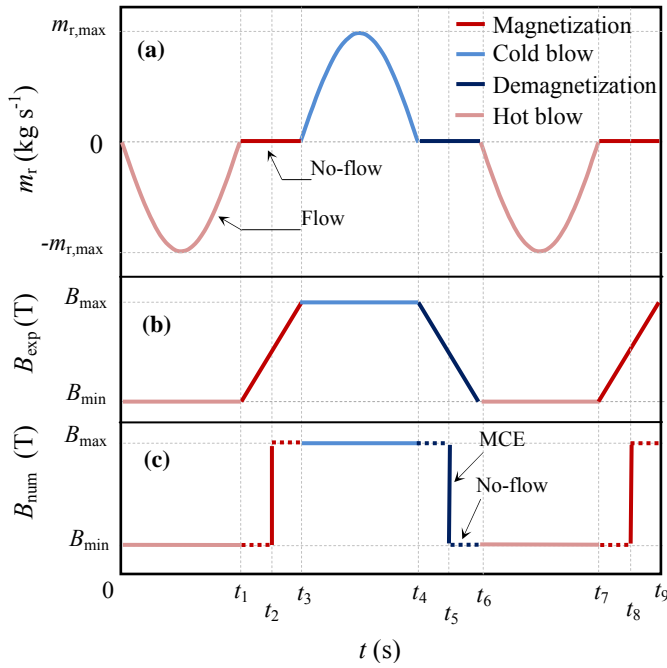


Figure 6 Variations of (a) m_r , (b) B_{exp} and (c) B_{num} with time t

Table 2 Mesh independence study at $\delta_x/d = \delta_y/d = 1.5$, $L/d = 90$, $Re = 500$, $Pr = 7.0$

$n_{\Delta x}$	$n_{\Delta y}$	$n_{\Delta z}$	n_{CV}	Nu_{av}
8	8	60	24480	5.71
8	8	90	36720	5.70
8	8	120	46080	5.58
8	8	150	57600	5.59
10	10	60	37200	5.59
10	10	90	55800	5.57
10	10	120	74400	5.55
10	10	150	93000	5.64
15	15	60	48960	5.59
15	15	90	73440	5.57
15	15	120	97920	5.55
15	15	150	122400	5.54

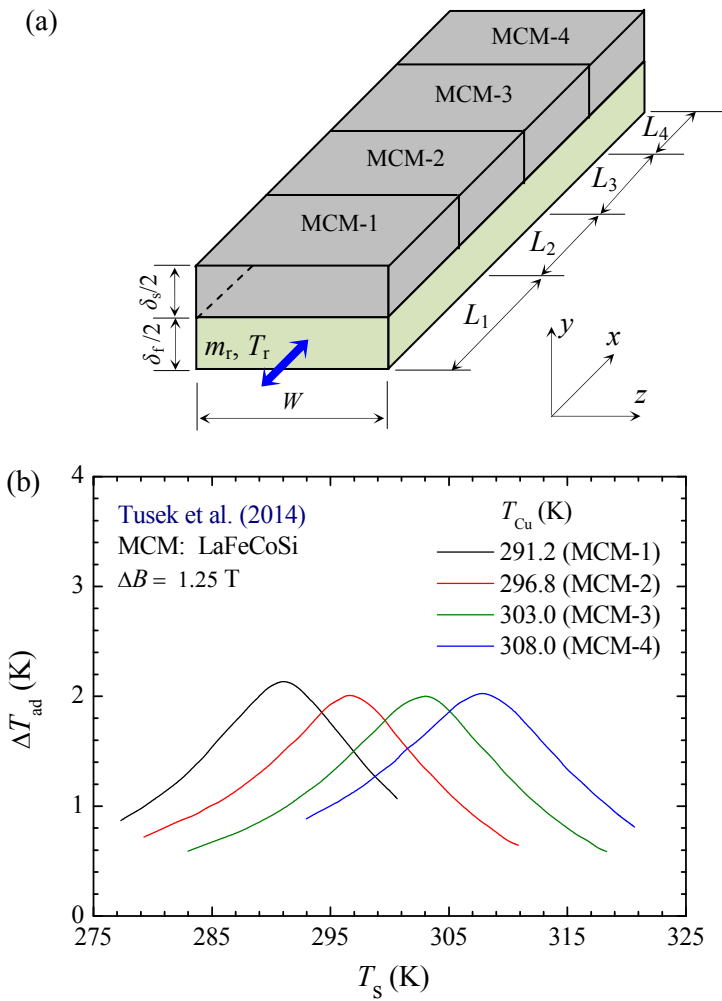
4. Results and discussion

The models and code validation and parametric study to optimise system performance are carried out. The results are discussed below.

4.1 Comparison with experimental data

The validation of the present numerical method for multiple-MCM regenerator is performed by comparing the simulation results with the experimental data of Tusek et al. [10] and Legait et al. [11] parallel-plate regenerators made of four different $\text{LaFe}_{13-x-y}\text{Co}_x\text{Si}_y$ compounds. **Figure 7(a)** shows the physical model of parallel-plate regenerator with four MCMs. The variation of ΔT_{ad} with temperature for the cases of Tusek et al. [10] and Legait et al. [11] are shown in **Figure 7(b)** and **7(c)**.

Single Column Figure



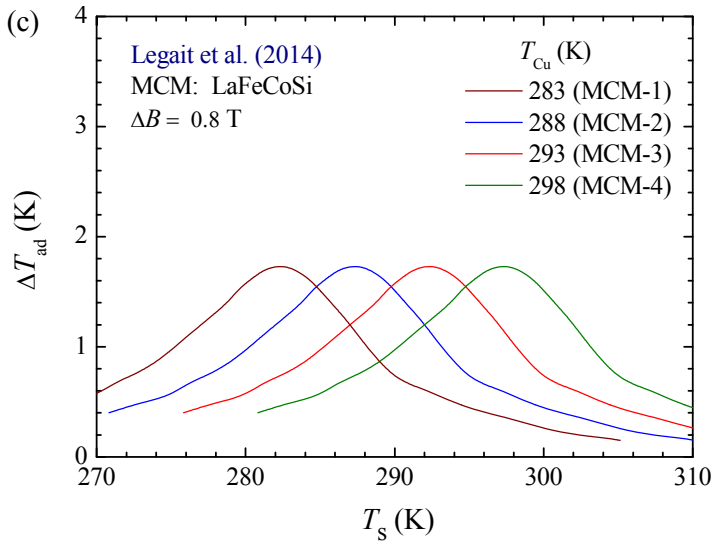


Figure 7 (a) Physical model of the parallel-plate regenerator with 4 MCMs; (b) Variation of ΔT_{ad} with temperature for four $\text{LaFe}_{13-x-y}\text{Co}_x\text{Si}_y$ compounds with different T_{Cu} used in experiment by Tusek et al. [10] with $T_{Cu} = 291.2, 296.8, 303.0$ and 308.0 K; (c) Variation of ΔT_{ad} with temperature for four $\text{LaFe}_{13-x-y}\text{Co}_x\text{Si}_y$ compounds used in experiment by Legait et al. [11] with $T_{Cu} = 283, 288, 293$ and 298 K.

Legait et al. [11] conducted experimental investigations of single and multi-MCM parallel-plate regenerators made of different alloys of $\text{LaFe}_{13-x-y}\text{Co}_x\text{Si}_y$. **Figure 8** compares the no-load temperature spans for the experimental data of Legait et al. [11] and the present numerical results under same operating conditions. The simulation was initialised with a linear initial gradient in the regenerator solid and channel to save computational time. **Figure 8(a)** shows the transient development of temperature span for $\varphi = 0.1$. The steady-state temperature span of ~ 13 K is predicted by the model while the corresponding experimental value is ~ 10.5 K. It can be seen that the model can predict results within an average difference of 25% from the experimental data.

Single Column Figure

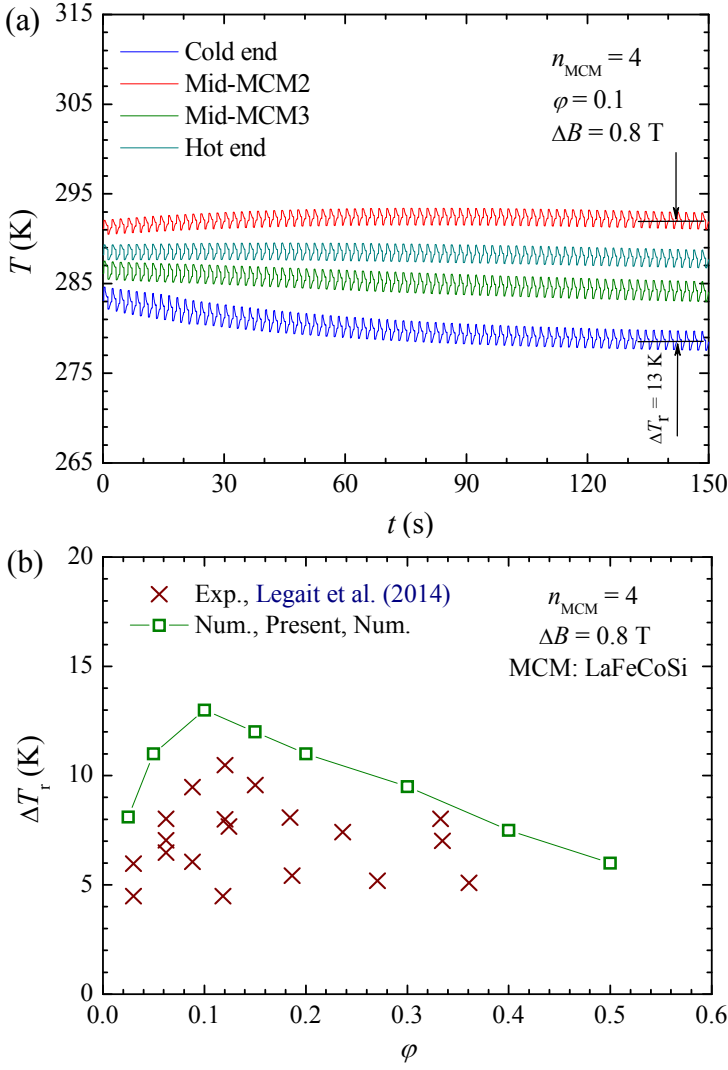


Figure 8 Comparison of the present results with experimental data of Legait et al. [11] with four $\text{LaFe}_{13-x-y}\text{Co}_x\text{Si}_y$ compounds having $T_{\text{Cu}} = 283, 288, 293$ and 298 K: (a) no-load temperature for $\varphi = 0.1$; (b) variation of temperature span with utilization.

Similarly, numerical results are compared with the experimental data of Tusek et al. [10] for four MCM based parallel plate regenerator and presented in **Figure 9**. The transient response of four-MCM regenerator for $\varphi = 0.1$ is shown in **Figure 9(a)** giving a temperature span of ~ 23 K. The no-load temperature spans predicted by numerical model are plotted with the experimental results of Tusek et al. [10] in **Figure 9(b)**. The maximum difference between the numerical predictions and the experimental data is $\sim 30\%$. The main sources causing the deviation of numerical results from the experimental data are the assumptions of negligible parasitic heat losses to surrounding, absence of internal demagnetising field and few other simplifications made in the development of the present model. Also, the MCE calculated using the mean field model is slightly larger than the

corresponding experimental values and this it is another cause of the over-predicted numerical results.

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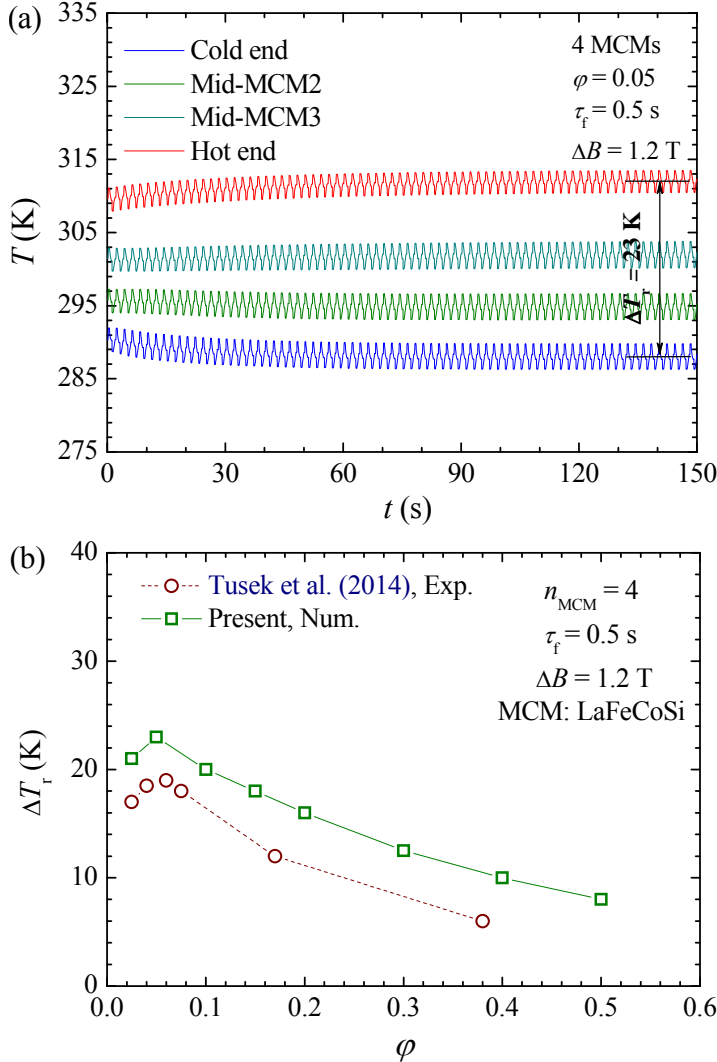


Figure 9 Comparison of the present results with experimental data of Tusek et al. [10] with four LaFe_{13-x-y}Co_xSi_y compounds having $T_{\text{Cu}} = 291.2, 296.8, 303.0$ and 308.0 K; (a) no-load temperature for $\varphi = 0.05$; (b) variation of temperature span with utilization.

An estimation of the heat losses to environment is made using the following set of equations (Nielsen et al. [30]).

$$Q = \frac{\Delta T}{R_{\text{tot}}} \quad (26)$$

where ΔT is the temperature difference between the local temperature of the MCM regenerator $T_{r,i}$ along the flow direction and the ambient temperature T_∞ .

$$R_{\text{tot}} = R_{\text{MCM}} + R_{\text{hou.}} + R_{\text{conv.}} \quad (27)$$

where R_{MCM} and $R_{\text{hou.}}$ are the conductive thermal resistances of the MCM and the regenerator housing respectively and R_{conv} is the convective resistance. The thermal conductivity of the MCM is taken as $10.6 \text{ Wm}^{-1}\text{K}^{-1}$ (that of Gd) and for the regenerator housing the thermal conductivity is $0.2 \text{ Wm}^{-1}\text{K}^{-1}$ for the calculation of R_{MCM} and $R_{\text{hou.}}$. The value of natural convection coefficient is taken as $15 \text{ Wm}^{-2} \text{K}^{-1}$ to calculate R_{conv} (Cengel [27], Holman [31]).

Figure 10 shows the comparison of the present simulation results with and without heat losses and the experimental data of Tusek et al. [10]. It can be seen that with the inclusion of the heat losses in the present numerical model, the maximum difference between the experimental and numerical results reduces to $\sim 15\%$.

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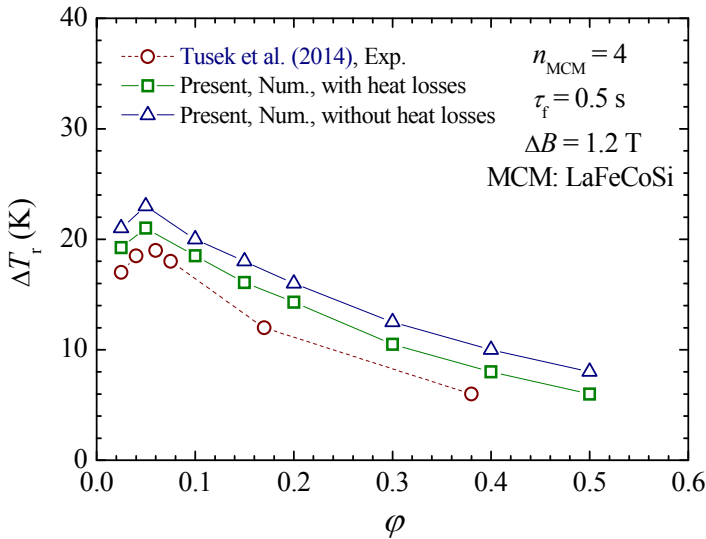


Figure 10 Comparison of the present simulation results with and without heat losses and the experimental data of Tusek et al. [10] with four $\text{LaFe}_{13-x-y}\text{Co}_x\text{Si}_y$ compounds having $T_{\text{Cu}} = 291.2, 296.8, 303.0$ and 308.0 K.

4.2 Parametric study on microchannel regenerator

Microchannel regenerator shown in **Figure 3** is used in the following sections to predict the performance under different geometric dimensions and operating conditions. The operating and

geometric conditions for various components of the magnetic refrigerator model are listed in **Table 3**. Two cases of the microchannel regenerator A and B are summarised in **Table 4**. The overall regenerator size is taken as 30 mm × 21 mm × 90 mm. The regenerator porosity ε and the specific heat transfer area a_p are changed by changing microchannel diameter d_{ch} , inter-channel (centre to centre) spacing δ_{ch} and number of channels n_{ch} for the two cases.

Table 3 Dimensions and parameters for microchannel (MCM: Gd; overall dimensions 30 mm × 21 mm × 90 mm).

Component	Geometric/operating conditions
Regenerator	Gd and its hyp. alloys, 21 mm × 30 mm × 90 mm, $d_{ch} = 1.0$ mm, 1.5 mm.
Working fluid	Water, $\lambda_f = 0.6$ Wm ⁻¹ K ⁻¹ , $c_f = 4180$ Jkg ⁻¹ K ⁻¹ , $\rho_f = 1000.0$ kgm ⁻³
Auxiliary fluids	Water
Magnet	Material: NdFeB, size: 100 mm × 50 mm × 25 mm, $\Delta B = 0.8$ T, 1.0 T.
CHEX	$d_{i,c} = 4.0$ mm, $d_{o,c} = 6.0$ mm, $l_c = 250.0$ mm, $m_c = 250$ gs ⁻¹ .
HHEX	$d_{i,h} = 4.0$ mm, $d_{o,h} = 6.0$ mm, $l_h = 250.0$ mm, $m_h = 250 - 500$ gs ⁻¹
Displacer	Displacer: $d_p = 16$ mm, $l_s = 2R = 10 - 100$ mm, $\omega = f$ (f)

Table 4 Dimensions and parameters for microchannel regenerators (MCM: Gd; overall dimensions 30 mm × 21 mm × 90 mm)

Case	d_{ch} mm	δ_{ch} mm	n_{ch}	d_h mm	ε	a_p m ² m ⁻³	m_s g
A	1.0	1.2	400	1.0	0.50	1995	225
B	1.5	1.7	176	1.5	0.50	1316	227

4.2.1 No load temperature span

Figure 11(a) plots the transient development of temperature span for single and three-MCM regenerators. The Curie temperatures are taken to be 284.0 K, 289.0 and 294.0 K and their respective ΔT_{ad} -vs- T_s profiles are shown in **Figure 5(a)**. As can be seen in **Figure 11(a)**, a larger temperature span by ~9 K is achieved using a three-MCM regenerator as compared to single-MCM regenerator at a cycle frequency of 2.0 Hz. **Figure 11(b)** plots the variation of no-load temperature span with utilization for the two regenerators for $f = 0.5$ Hz. The no-load temperature span decreases as the utilization is increased and the difference in the performance of two regenerators also decreases. The cooling capacity of the system is directly related to the established temperature

span along the length of the regenerator. Thus, larger temperature span corresponds to improved performance of the magnetic refrigerator.

Single Column Figure

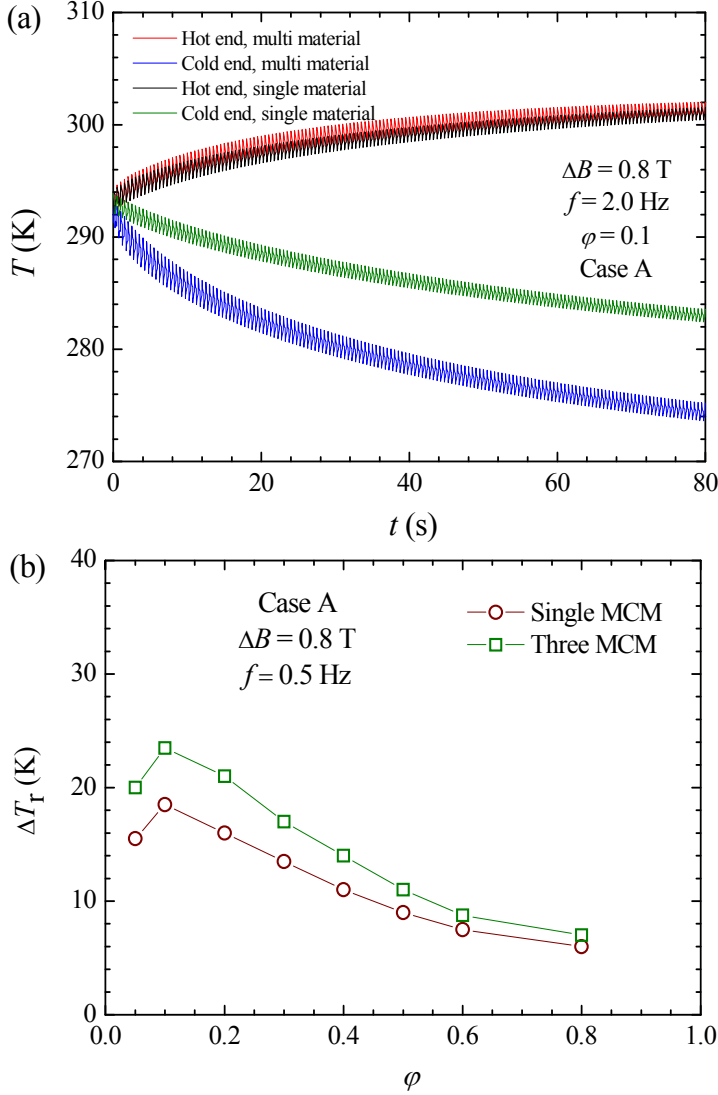


Figure 11 (a) Transient response of single and three-MCM microchannel regenerator for case B (see **Table 4**) $\Delta B = 0.8$ T, $f = 0.5$ Hz; (b) Variation of no-load temperature span ΔT_r with utilization for single MCM and three-MCM based regenerators (hypothetical materials).

4.2.2 Effect of number of MCMs

Utilization depends upon the specific heat capacity of the MCM as can be seen in Eq. (25). For single-MCM regenerator, the material considered was Gd with known c_p of $290 \text{ J kg}^{-1} \text{ K}^{-1}$ (at $B = 0$ T, $T = T_{Cu}$) and utilization is calculated using this value. However, for the case of multiple MCM, utilization would be determined by the average of heat capacities of different MCMs employed in the regenerator (Nielsen [32]). As MCMs with hypothetical T_{Cu} have been considered, a simplifying assumption is made and

utilization is calculated by taking the average heat capacity of different MCMs to be the same as that of Gd. The assumption is reasonable due to minor variation of magnetocaloric properties with change in Curie temperature in the range 280-300 K (email discussion with Dr. Matthias Katter, Vacuumschmelze GmbH).

Figure 12 compares the variations of cooling capacity with utilization for single and three-MCM regenerators. For three-MCM microchannel regenerator, two hypothetical MCMs with Curie temperatures of 284 K and 289 K are considered with Gd as the third MCM as shown in **Figure 5(a)**. The cooling capacity of three-MCM regenerator is larger than single-MCM and the difference in the corresponding peak values is ~25%.

Single Column Figure

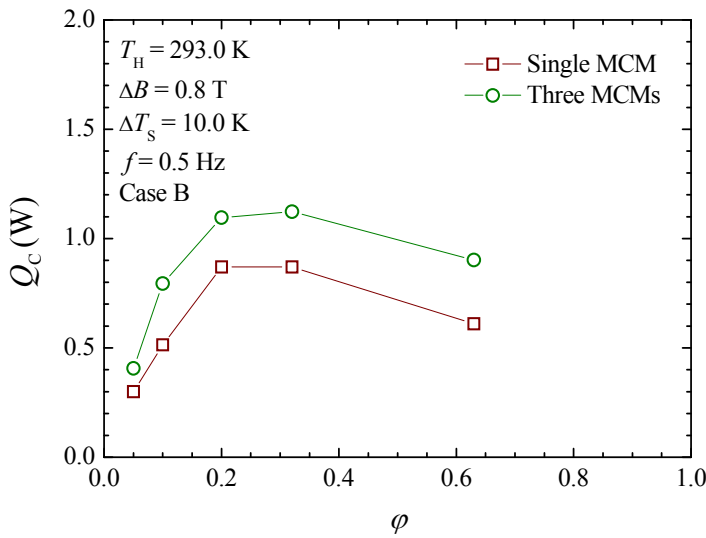


Figure 12 Variation of cooling capacity with utilization for single and three MCM based regenerators for microchannel regenerator Case B (see **Table 4**), $T_H = 293.0$ K; $\Delta B = 0.8$ T, $f = 0.5$ Hz.

Figure 13(a) shows three cases of microchannel regenerator with different number of MCMs. Single MCM regenerator has $T_{Cu} = 294.0$ K. For multi-MCM cases, Curie temperature difference is kept to be 4.0 K between any two consecutive MCMs. Thus, two-MCM regenerator has T_{Cu} of 290.0 K and 294.0 K. For three-MCM case, T_{Cu} are taken to be 286 K, 290 K and 294 K while for the four-MCM case T_{Cu} are 282 K, 286 K, 290 K and 294 K. The three cases are numerically simulated for 1.0 T change in magnetic field, 0.5 Hz operating cycle frequency and hot end temperature was fixed to 293.0 K.

The variation of cooling capacity with utilization for different number of MMCs is plotted in **Figure 13(b)**. The cooling capacity is found to increase as the number of MCMs is increased for the given cases. For single MCM case, peak cooling capacity is at $\phi = 0.1$, while for two and three MCM cases the peaks are seen

at $\phi = 0.4$ and are $\sim 13\%$ and $\sim 28\%$ higher compared with peak capacity of single MCM regenerator, respectively.

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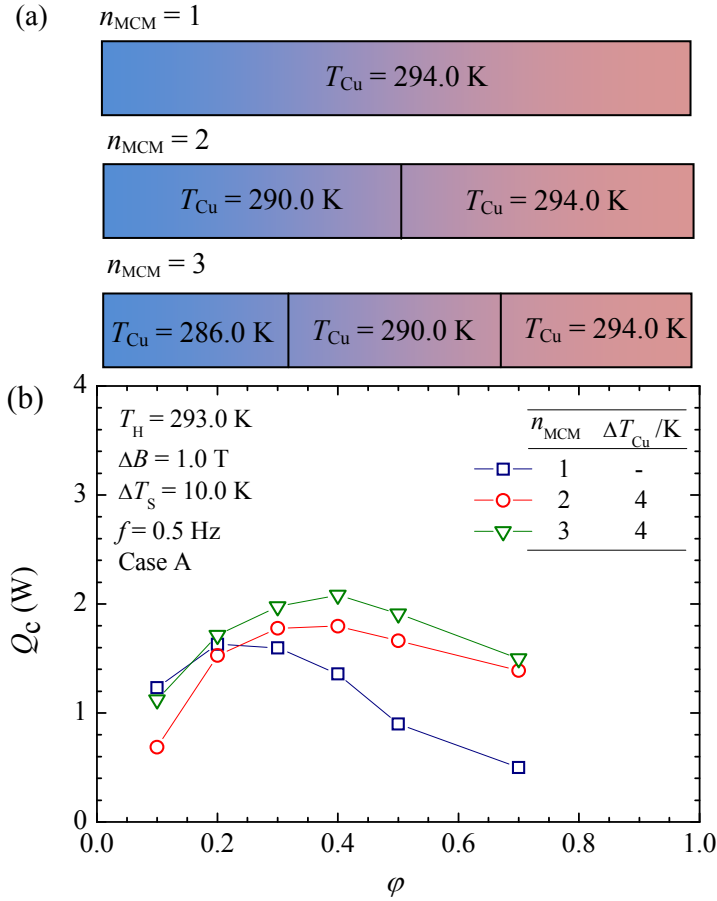


Figure 13 (a) Multi-MCM regenerators with different number of MCMs for $\Delta T_{\text{Cu}} = 4 \text{ K}$; (b) Variation of cooling capacity with utilization for no. of MCMs.

4.2.3 Effect of Curie temperature difference

The effect of Curie temperature difference ΔT_{Cu} between two adjacent MCMs is investigated. **Figure 14(a)** shows four cases of two-MCM regenerator with different ΔT_{Cu} value of 24.0 K, 16.0 K, 8.0 K, 4.0 K respectively. The MCM at the hotend is assigned $T_{\text{Cu}} = 294.0 \text{ K}$ (Gd) in all four cases while T_{Cu} of the second MCM is different in each case in order to obtain different ΔT_{Cu} values.

The cooling capacity curves for different values of ΔT_{Cu} are plotted in **Figure 14(b)**. For a given number of MCMs, cooling capacity increases as the ΔT_{Cu} decreases. This behaviour is mainly due to the dependence of temperature *jump* ΔT_{ad} (rise and drop) during magnetisation and demagnetisation on the local temperature T_{s} of the MCM solid (can be seen in **Figure 5**). To operate at room temperature 293.0 K, the MCM with T_{Cu} closer to 293.0 K (in this case Gd with $T_{\text{Cu}} = 294.0 \text{ K}$) experiences larger temperature change ΔT_{ad} while

MCM with T_{Cu} farther from 293.0 K will undergo relatively smaller temperature change. The MCM with $T_{Cu} = 270.0$ K (**Figure 5(a)**) experiences smaller temperature change during magnetisation/demagnetisation as its local temperature being 293.0 K and it can be seen from the ΔT_{ad} curve of $T_{Cu} = 270$ K in **Figure 5(b)** the temperature change is ~ 1 K at temperature of 293.0 K. However, if ΔT_{Cu} is decreased the difference in the temperature of the MCM and its Curie temperature also decreases which results in larger MCE/ ΔT_{ad} . The relative larger MCE yields improved performance.

Single Column Figure

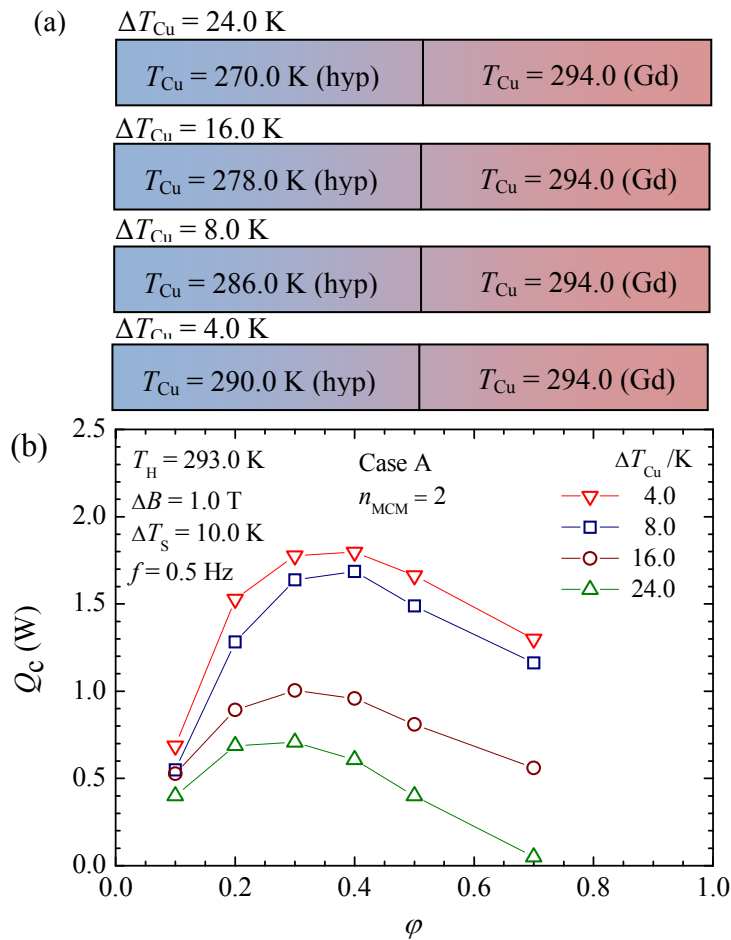


Figure 14 (a) Different cases of ΔT_{Cu} for two-MCM regenerator; (b) Variation of Q_c with utilization for different values of ΔT_{Cu} for two-MCM regenerator.

4.2.4 Effect of hot end temperature

For cooling purpose, the temperature of the hot end is kept constant while temperature at cold end is allowed to drop to be able to absorb heat from cooling load. The cooling capacity is sensitive to the hot side temperature and its influence is investigated by fixing hot end to different temperatures. For two-MCM

regenerator, the Curie temperatures are taken as 290.0 K and 294.0 K, and for the case of three MCMs the Curie points are considered to be 286.0 K, 290.0 and 294.0 K as can be seen in **Figure 13(a)**.

The variation of cooling capacity with the temperature of hot end T_H is shown in **Figure 15**. For single-MCM regenerator, the peak performance is seen when temperature of the hot end is fixed at 295.0 K i.e. near the Curie temperature of the employed MCM which is 294.0 K. The cooling capacity drops nearly at the same rate on either side of the cooling capacity peak for $T_H > 295.0$ and $T_H < 295.0$ for single MCM regenerator.

For two and three-MCM cases the peak performance is still seen around $T_H = 295.0$ K. However, the drop in the cooling capacity with T_H on either side of the peak follows different trends. For $T_H < 295.0$ K, the cooling capacity gradient with hot side temperature ($\partial Q_c / \partial T_H$) of three-MCM regenerator is much smaller compared with that of the two-MCM regenerator. Also, three-MCM regenerator gives ~50% higher cooling capacity than single-MCM and ~20% than two-MCM regenerator at $T_H = 285.0$ K. The main reason for the improved performance of three-MCM regenerator at $T_H = 285.0$ K is the presence of the MCM with $T_{Cu} = 286.0$ K which is, of course, not available in single and two-MCM regenerators. Similarly, the steeper decline of Q_c with T_H of three-MCM regenerator for $T_H > 295.0$ K can be reduced by the addition of MCMs with $T_{Cu} > 294.0$ K and the performance can be uplifted for higher T_H (which is advantageous for the ambient temperatures above 300 K).

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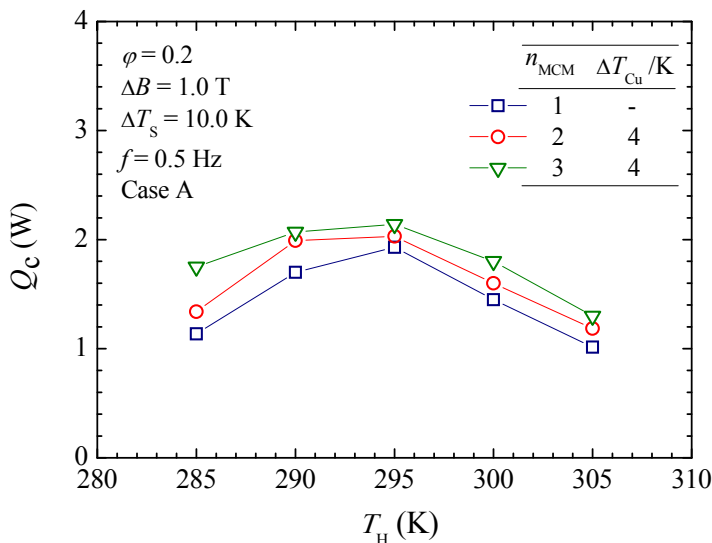


Figure 15 Multi-MCM regenerators with different number of MCMs with $\Delta T_{Cu} = 4$ K between two adjacent MCMs; (b) Variation of cooling capacity with hot side temperature for different number of materials.

5. Conclusions

A hybrid numerical model of a magnetic refrigerator was developed to simulate parallel-plate and microchannel regenerators made of multi-MCMs. The transient thermo-hydraulic response of active magnetic regenerators made of multiple MCMs was simulated using finite volume method based commercial software. The rates of heat transfer at cold and hot end heat exchanger were calculated using ϵ -NTU method. MCMs were considered with different Curie temperatures both for the commercially available compounds of $\text{LaFe}_{13-x-y}\text{Co}_x\text{Si}_y$ and hypothetical compounds of Gd. Discrete method was used for the incorporation of the magnetocaloric effect. Method/model validation was performed with experimental data available in the literature for parallel regenerators made of different compounds of $\text{LaFe}_{13-x-y}\text{Co}_x\text{Si}_y$. The model can predict results with a maximum difference of $\sim 15\%$ from the experimental data. Multi-MCM based regenerator have shown improved performance as compared to single MCM based regenerator. Cooling capacity was seen to increase as the number of MCMs increase, however, for a given length of regenerator there exists an optimum number of materials to obtain the maximum performance. For given number of MCMs, an optimum difference in Curie temperatures of two consecutive MCMs is found to yield improved performance compared with larger ΔT_{Cu} .

Acknowledgments

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Nomenclature

A	heat transfer area
a_p	heat transfer area per unit volume/specific heat transfer area
B	intensity of magnetic field
ΔB	maximum change in intensity of magnetic field
C	ratio of specific heat capacities

c_p	isobaric specific heat capacity
d	diameter
d_i	inside diameter
d_h	hydraulic diameter
d_o	outside diameter
d_p	cross-sectional diameter of piston
f	cycle frequency; rotational frequency; friction factor
l	length
L	length
m	mass; magnetization
m_r	mass flow rate in regenerator loop
n	number
\mathbf{n}	vector normal to boundary
P	pressure
q	heat flux
Q_c	heat exchange at CHEX
Q_h	heat exchange at HHEX
R	radius of crank disk of displacer
t	time
Δt	time step
T	temperature
T_{Cu}	Curie temperature
ΔT_r	temperature span between two ends of regenerator
\mathbf{u}	velocity vector
u	velocity in x -direction; mean velocity
U	overall heat-transfer coefficient
V	volume
v	velocity in y -direction

w velocity in z-direction

Greek

α thermal diffusivity

δ spacing; thickness

Δ change; difference

ε porosity; effectiveness; error $\varepsilon = (\Delta T_{r,num} - \Delta T_{r,exp}) / \Delta T_{r,exp} \%$

λ thermal conductivity

μ dynamic viscosity

ρ density

τ period of a cycle

ω angular velocity of the crank disk

Subscript

ad adiabatic

b bulk

c cold

cf counter-current flow

ch channel

ele electronic

exp experiment

f fluid

h hot, hydraulic

i inside

init initial

in inlet

j r, h or c

lat lattice

mag	magnetic
max	maximum
min	minimum
num	numerical
o	outside
out	outlet
pl	plate
r	regenerator
s	solid
tot	total
w	wall

Acronyms

AMR	active magnetocaloric regenerator
CHEX	cold and heat exchanger
COP	coefficient of performance
HHEX	hot end heat exchanger
MCE	magnetocaloric effect
MCM	magnetocaloric material
NTU	number of transferred units
UDF	user-defined function

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