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5th United Kingdom & Éire OpenFOAM® User Meeting  
16th-17th January 2017  
University College Dublin

# A hybrid slurry CFD model: Euler-Euler to Euler-Lagrange (in development)

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# Outline

- ♦ Background, context and motivation to the problem
- ♦ Development of hybrid model will be explained
- ♦ Test case will be shown
  
- ♦ Tutorial can be found on Chalmers website (end of January):  
[http://www.tfd.chalmers.se/~hani/kurser/OS\\_CFD\\_2016/](http://www.tfd.chalmers.se/~hani/kurser/OS_CFD_2016/)

# Background

- ◆ Weir group produce equipment for the mining and oil and gas industries
- ◆ Erosion is a large problem
- ◆ CFD modelling is used to predict erosion = better designs
- ◆ Longer pump life = happy customer :)



# Impellers

**Before**



**After**

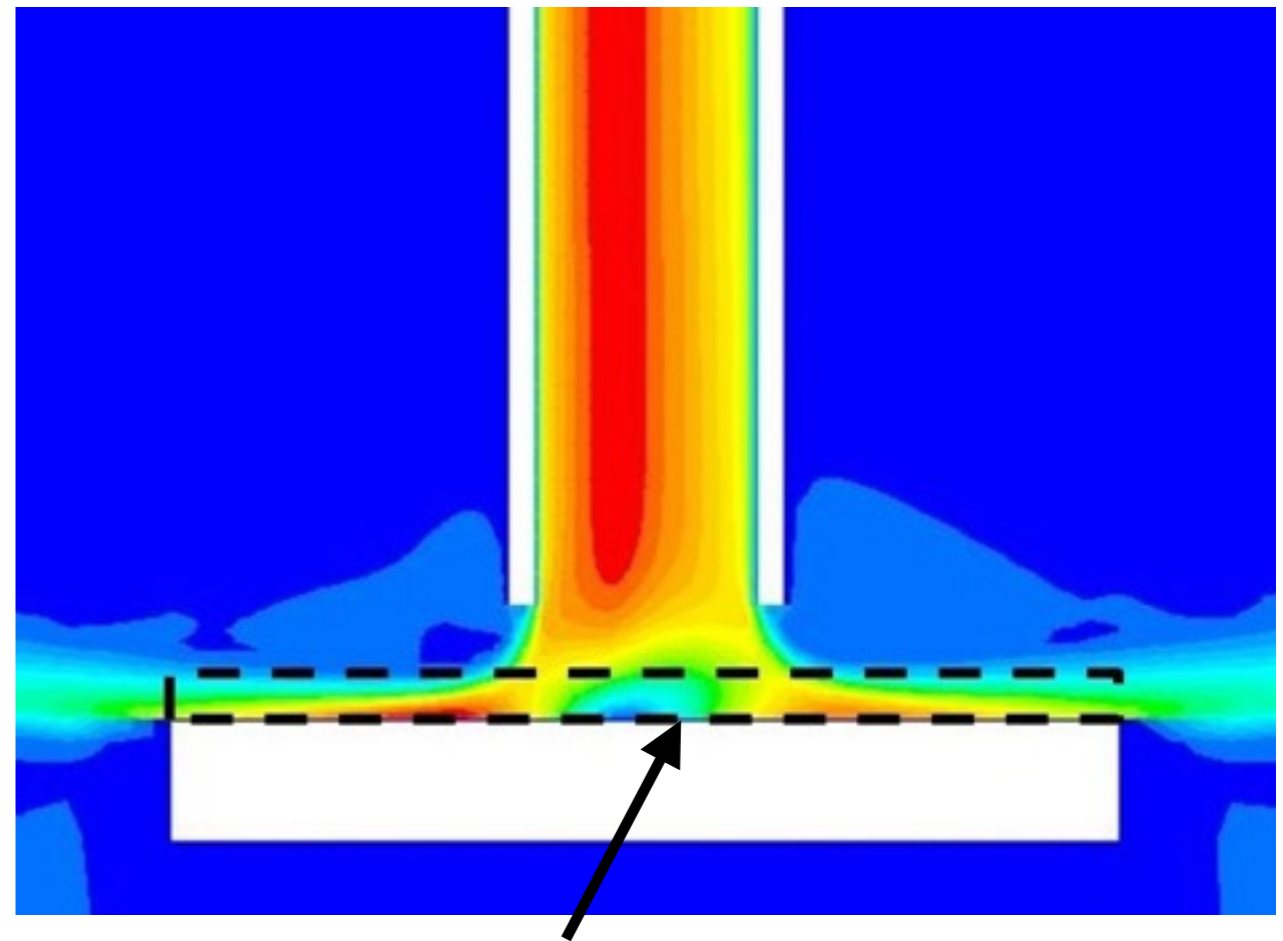


Could be as little as 2 weeks of continuous running for this to happen

# Problem/Motivation

- ◆ Need particle impact data at the wall for erosion modelling
- ◆ Fluid/particulate flow simulation is computationally expensive: especially for dense slurries
- ◆ Solution to make faster: Combine with two-fluid model

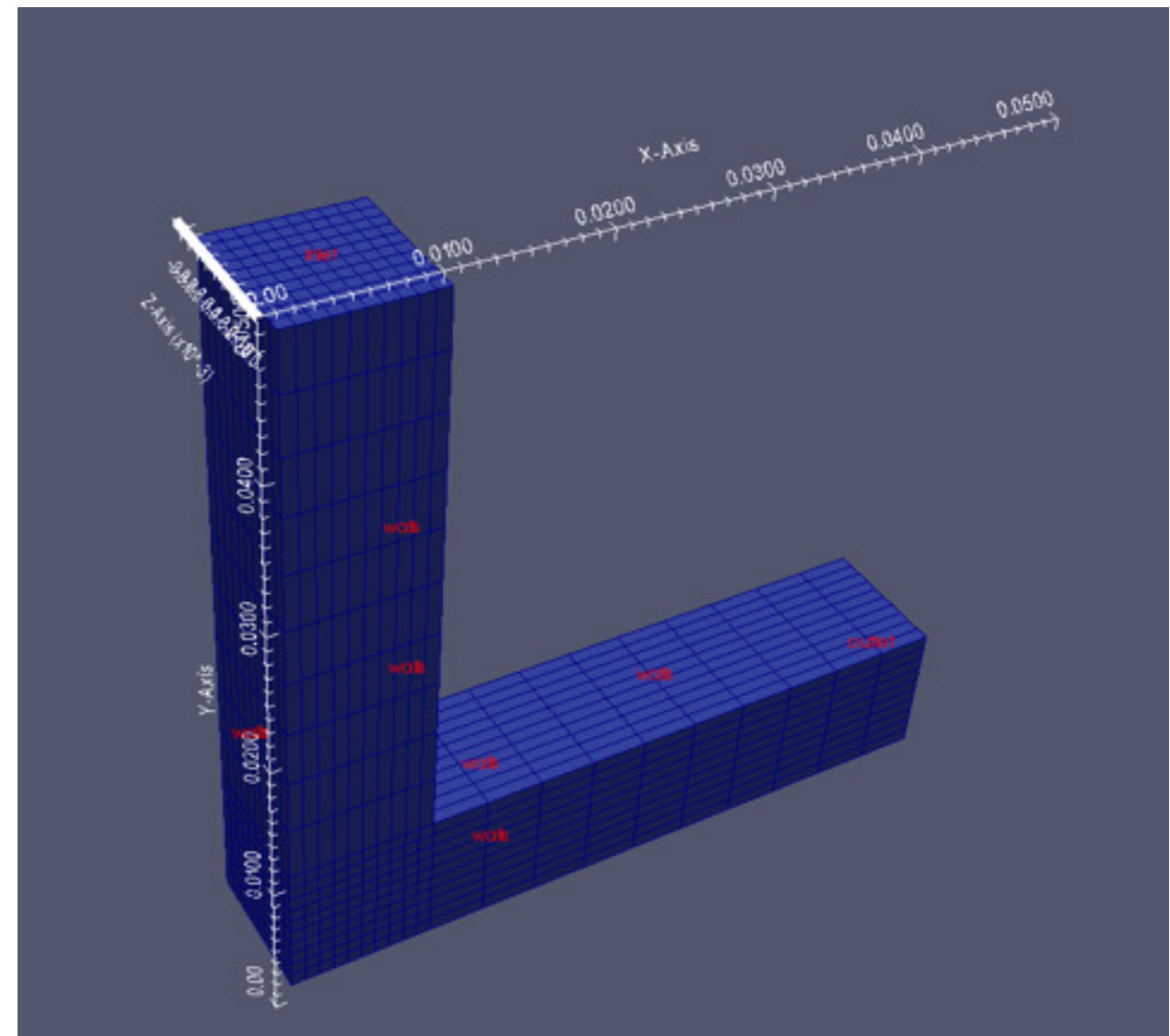
*Velocity contours of submerged jet impingement test*



Dotted region where particles are necessary for impact data

# Geometry and Solvers

- ◆ A simple geometry was chosen for solver development
- ◆ reactingTwoPhaseEulerFoam for Euler-Euler
- ◆ DPMFoam for Euler-Lagrange
- ◆ OpenFOAM 3.0.x was used



*Geometry shown with sizes in metres*

# Description of Solvers

reactingTwoPhaseEulerFoam

Euler-Euler

Two fluid model

Both phases treated as  
continuum

Incompressible model: setting in  
dictionary

Fast to solve

DPMFoam

Euler-Lagrange

Fluid/particle model

Transient solver for coupled  
transport of kinematic particle  
clouds

Includes the effect of volume  
fraction of the particles on the  
continuous phase

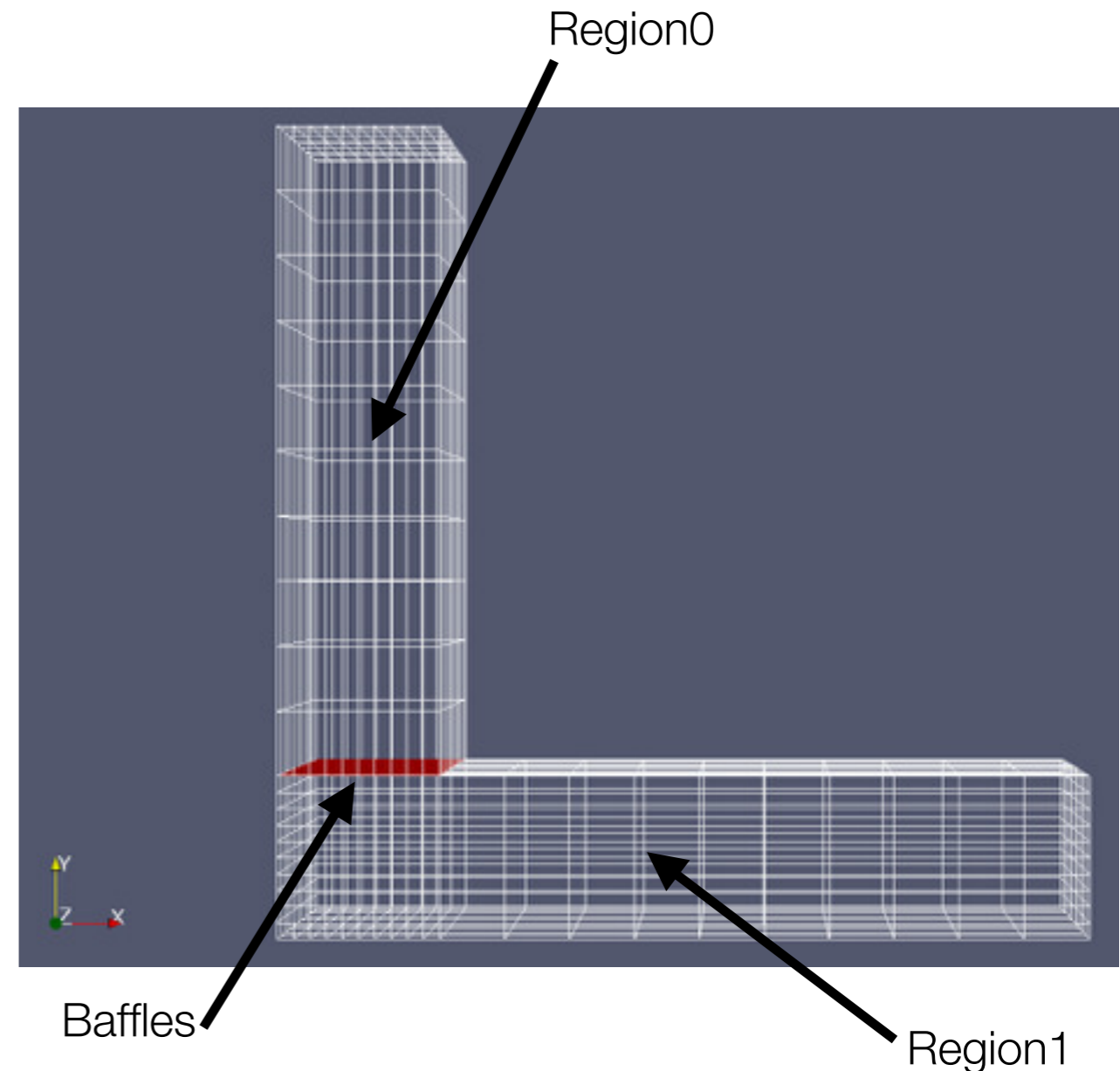


# Combining the solvers

- ♦ A new solver was made based on the EE model
- ♦ To have 2 solvers running, 2 regions were created
- ♦ To go from fluid to particles, we need a transition
- ♦ An outlet/inlet is needed for particle phase, but shouldn't affect the rest of the flow
- ♦ Solution...

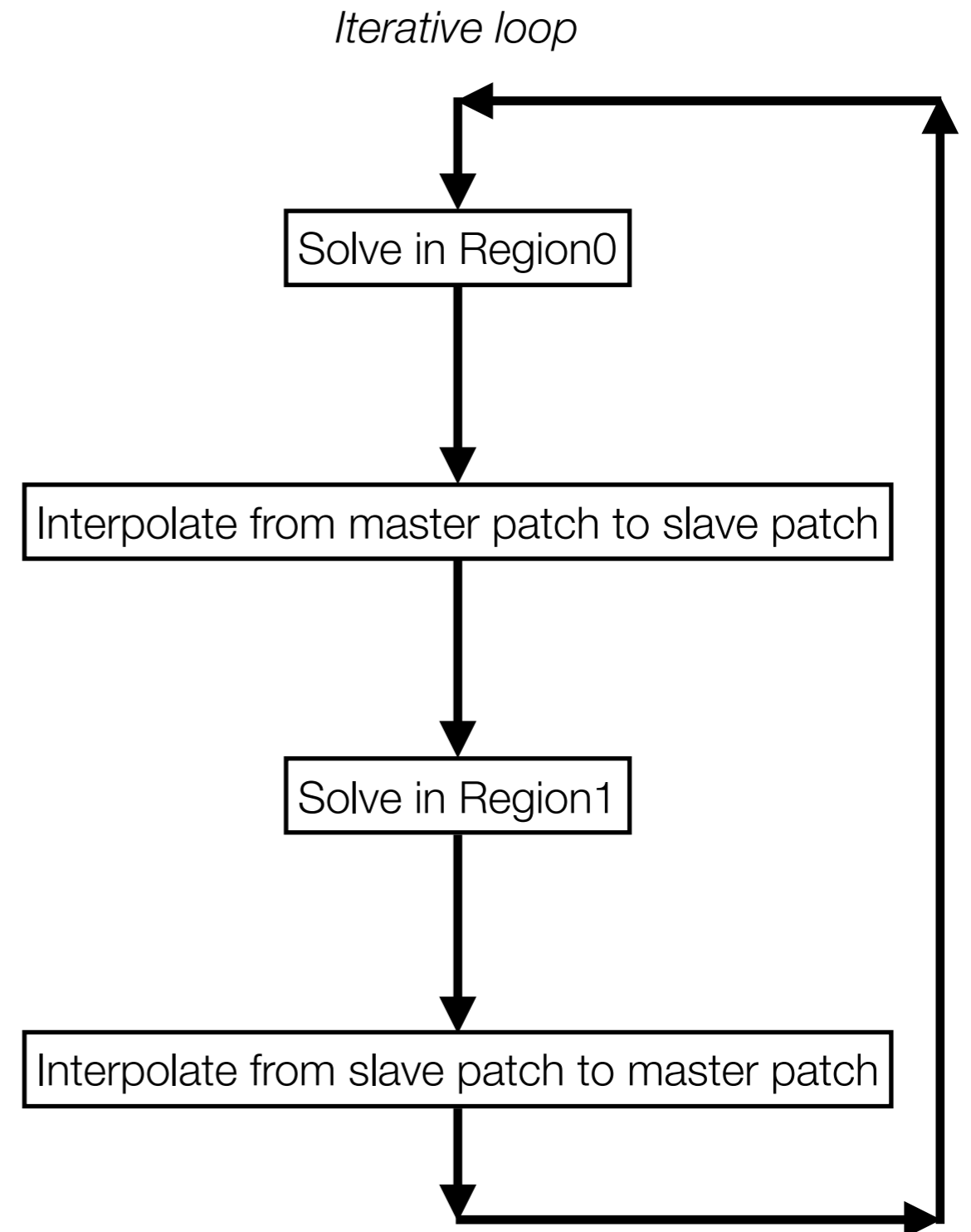
# Baffles + Regions

- ◆ `createBaffles`: makes internal surface into boundary face
- ◆ *master* and *slave* patch created
- ◆ `splitMeshRegions`: Splits mesh into 2 separate regions
- ◆ BC's can now be applied to baffle patches
- ◆ `chtMultiRegionFoam`: Inspiration for solving regions sequentially



# Interpolation

- ♦ `patchToPatchInterpolation`: transfers data between two patches
- ♦ All variables are interpolated:  $U_1$ ,  $U_2$ ,  $p$ ,  $p_{rgh}$ ,  $\alpha_1$ ,  $\alpha_2$ ,  $k$ ,  $\epsilon$ ,  $\nu$ , and  $\theta$
- ♦ After this is implemented, the domain runs as if it was one region, not two: the surface doesn't affect the flow
- ♦ 'back pressures' are taken into account by interpolating upstream



# DPMFoam added

- ◆ Code from DPMFoam was added to new solver
- ◆ Particles injected from slave patch after back interpolation (slave to master)
- ◆ Particles are only in region1 (near wall)
- ◆ Injection values based on phase 2 from region0 by using a lookup table: kinematicLookupTableInjection

# DPMFoam injection

```
18 /* (x y z) (u v w) d rho mDot numParcels
19     where:
20     x, y, z = global cartesian co-ordinates [m]
21     u, v, w = global cartesian velocity components [m/s]
22     d       = diameter [m]
23     rho     = density [kg/m3]
24     mDot    = mass flow rate [kg/m3]
25     numParcels = number of Parcels
26     Dictionary for the KinematicLookupTableInjection */
27 (
28 (0.0005 0.01 -0.0005) (0.01417 0.01831 -0.001718) 5.5e-05 2750 0.005 -2
29 (0.0015 0.01 -0.0005) (0.06206 -0.1608 -0.001616) 5.5e-05 2750 0.005 10
30 (0.0025 0.01 -0.0005) (0.1088 -0.3422 -0.0005019) 5.5e-05 2750 0.005 19
31 (0.0035 0.01 -0.0005) (0.1497 -0.4695 -0.001312) 5.5e-05 2750 0.005 24
```

- ✦ Modified kinematicLookupTableInjection used to inject particles
- ✦ Lookup table is updated every time step (but not read every time step: advice welcome!)
- ✦ 1 line = 1 cell (100 cells in this case)
- ✦ Values for particle injection are based on new updated values so solver can deal with geometry changes etc. See Lopez' presentation for more details:

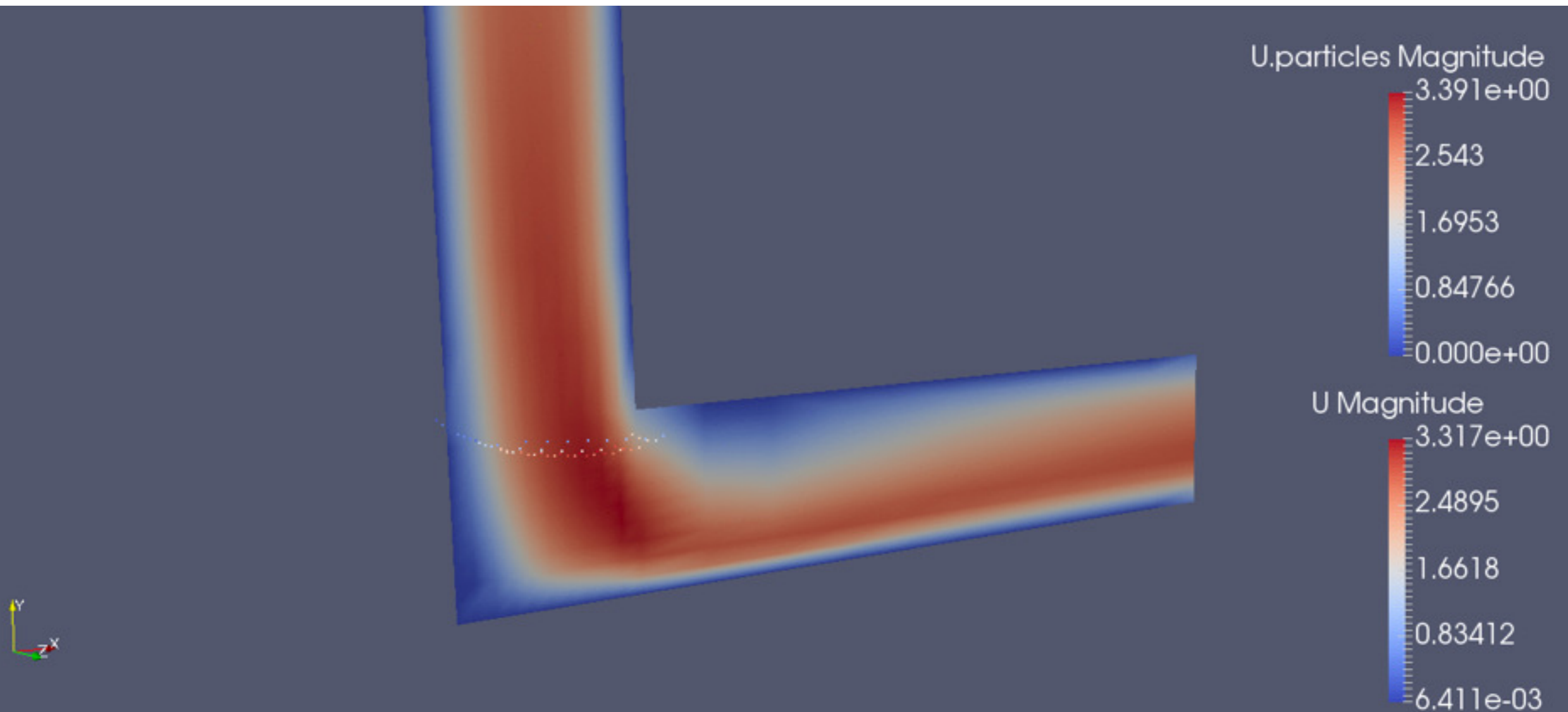
[https://sourceforge.net/projects/openfoam-extend/files/OpenFOAM\\_Workshops/OFW10\\_2015\\_AnnArbor/Presentations/Lopez-present-OFW10-16.pdf/download](https://sourceforge.net/projects/openfoam-extend/files/OpenFOAM_Workshops/OFW10_2015_AnnArbor/Presentations/Lopez-present-OFW10-16.pdf/download)

# DPMFoam injection

```
459 os <<"/* (x y z) (u v w) d rho mDot numParcels \n";
460 os <<" where: \n";
461 os <<" x, y, z = global cartesian co-ordinates [m] \n";
462 os <<" u, v, w = global cartesian velocity components [m/s] \n";
463 os <<" d = diameter [m] \n";
464 os <<" rho = density [kg/m3] \n";
465 os <<" mDot = mass flow rate [kg/m3] \n";
466 os <<" numParcels = number of Parcels \n";
467
468 os <<" Dictionary for the KinematicLookupTableInjection */ \n";
469 os <<"(" << endl;
470 forAll(interpolatedInletU1, i)
471 {
472 os << centres[i] <<" " << interpolatedInletU1[i] <<" " << 55e-6 <<" " << 2750 <<" " << 0.005 <<" "
<< floor ((alpha1[i]*(mag(normalSlaveVector[i]))*uNormal[i])/((8.71e-14)*3*(-1)*5000)) << endl; |
473 }
474 os <<"//The end"<< endl;
475 os <<");"<< endl;
```

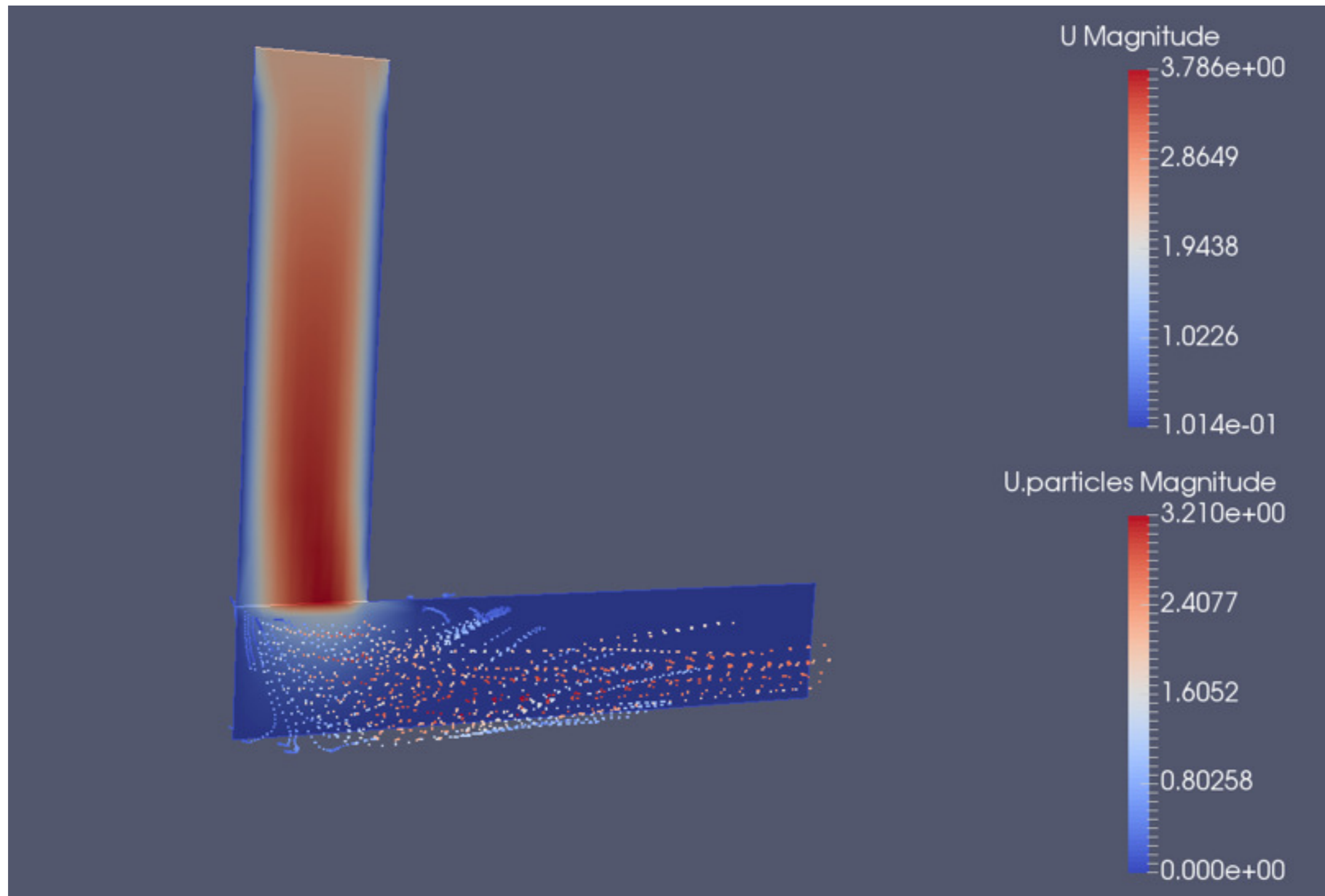
- ◆ Number of parcels to be injected is calculated from volume flow rate of 2nd phase of fluid.
- ◆ Number of parcels/cell = (alpha particles \* area of cell \* normal velocity component to cell boundary face) / (volume of one particle \* number of particles/parcel \* number of time-steps/second)

# Velocity contours



- ♦ 2D slice through Z normal. Particles injected from slave patch

# Velocity contours





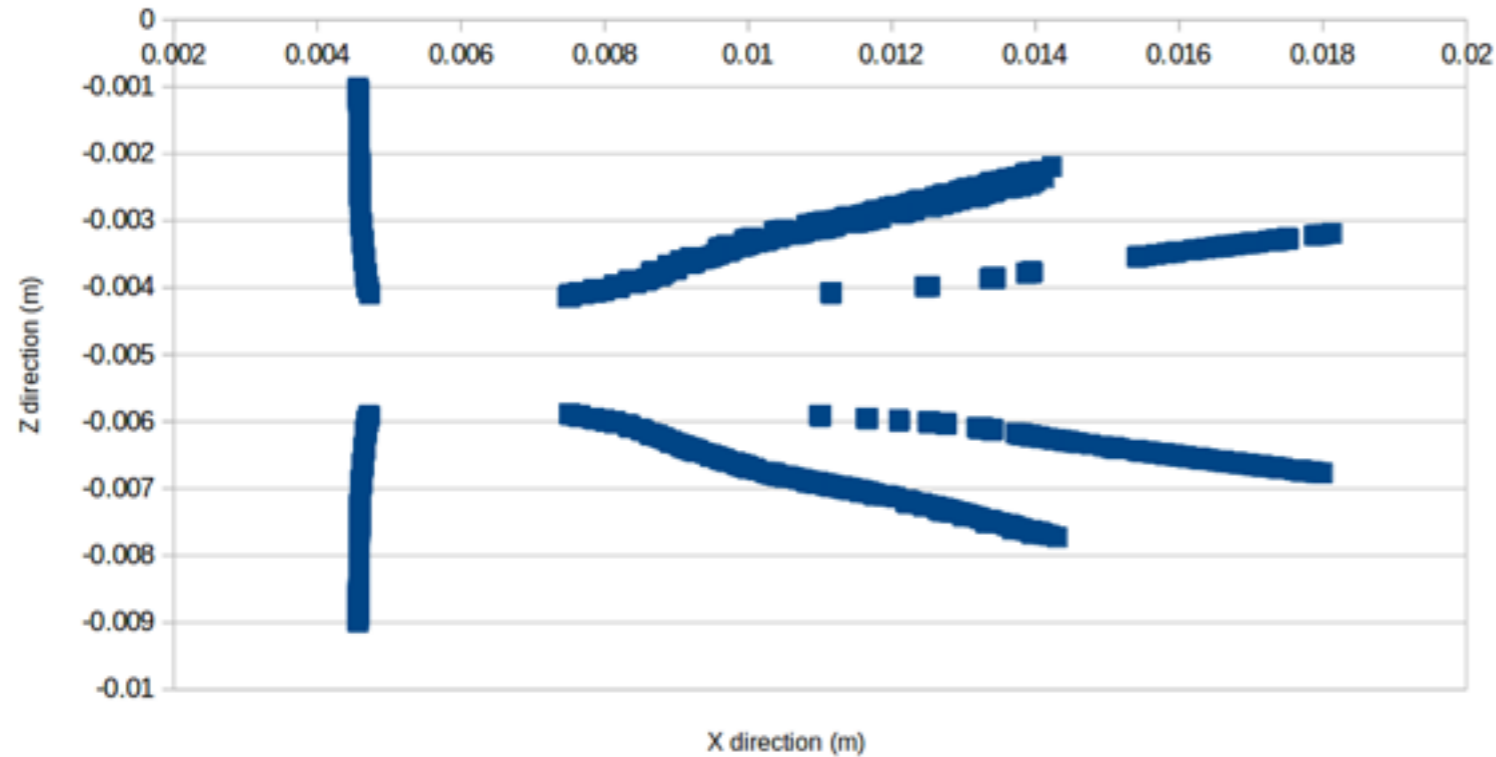
# Comparison

- ♦ New solver was compared against standard EL and EE solvers
- ♦ Hybrid model is almost double the speed of the EL

Execution time from 0-0.39s: % mass concentration (MC)

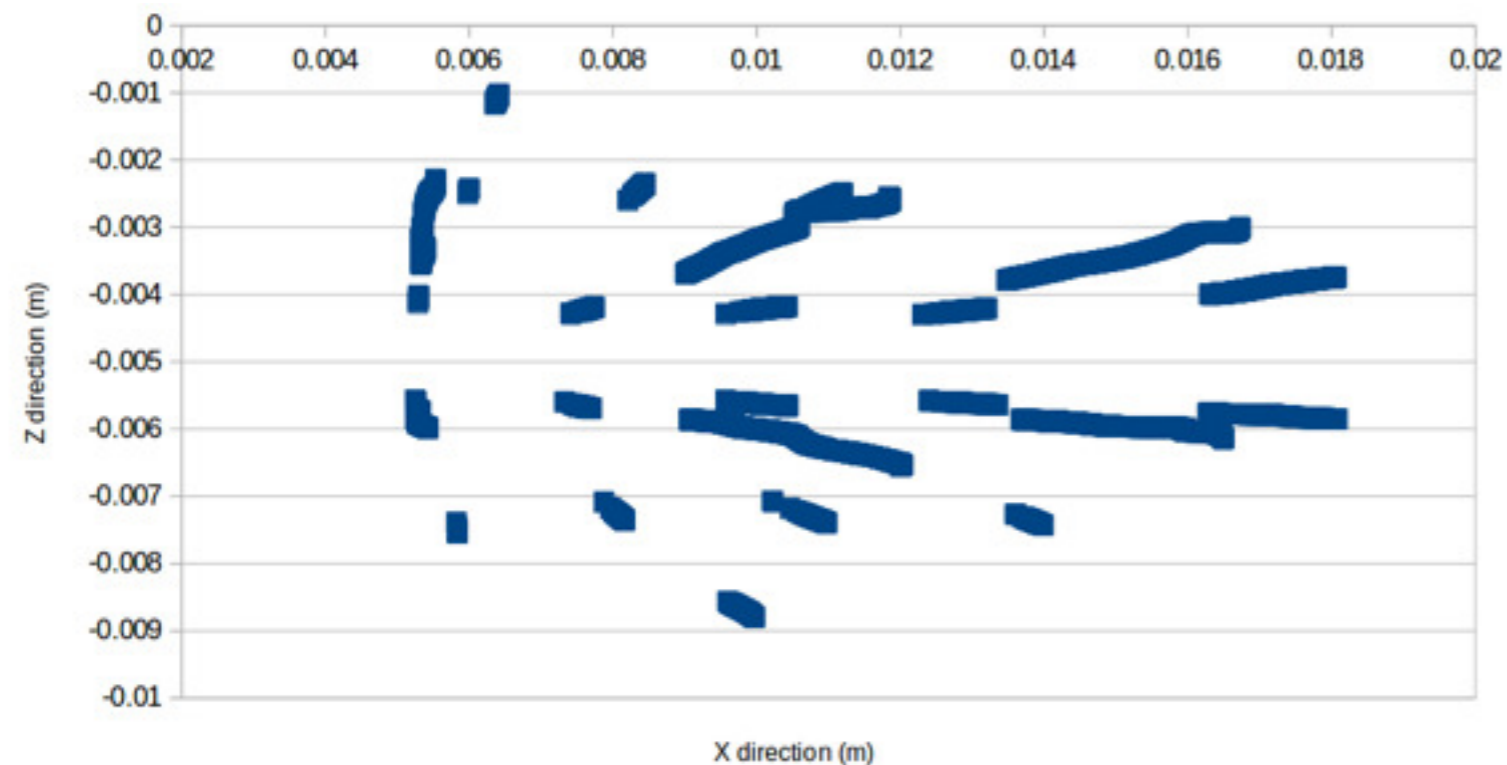
Model	Execution Time (s)	
	1% MC	2% MC
Hybrid model	225	298
Euler-Lagrange	420	585
Euler-Euler	102	105

# Comparison



Hybrid Model particle impacts

Data taken from bottom wall  
on pipe bend



DPMFoam particle impacts

# Future work

- ♦ Validation of hybrid model: CFD and experimental (PIV)
- ♦ Particles to fluid, for after region of interest...
- ♦ Move lookupTable to memory?
- ♦ Make solver re-read the lookupTable (suggestions welcome)

# Conclusion

- ◆ Solver should dramatically reduce computational time
- ◆ Particle data should still be present near walls, where required
- ◆ Enable better design of mining equipment



*Worn impeller of slurry pump*

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Thank you. Questions?

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