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**Pacific Northwest  
National Laboratory**

Operated by Battelle for the  
U.S. Department of Energy

## Estimate of Hanford Waste Rheology and Settling Behavior

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October 2007

Prepared for the U.S. Department of Energy  
under Contract DE-AC05-76RL01830



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Test specification: N/A  
Test plan: N/A  
Test exceptions: N/A  
R&T focus area: Pretreatment  
Test Scoping Statement(s): SCN 007

Pacific Northwest National Laboratory  
Richland, Washington, 99354

## Completeness of Testing

This report summarizes the results of analyses of data obtained from the referenced analyses of Hanford waste. The analyses and the report, which used data from, but did not involve laboratory testing, followed the quality assurance requirements outlined in Pacific Northwest Division's Waste Treatment Plant Support Project Quality Assurance Requirements and Description Manual and are now compiled under the quality assurance requirements of the PNNL River Protection Project – Waste Treatment Plant Support Program (RPP-WTP) Quality Assurance Plan, RPP-WTP-QA-001.

The descriptions provided in this report are an accurate account of both the conduct of the work and the data analyses performed. A summary of the analysis results is reported. Also reported are any unusual or anomalous occurrences that are different from expected results. The analysis results and this report have been reviewed and verified.

Approved:



Gordon H. Beeman, Program Manager  
RPP-WTP Support Program

10/26/07  
Date

# Testing Summary

The U.S. Department of Energy (DOE) Office of River Protection's Waste Treatment and Immobilization Plant (WTP) will process and treat radioactive waste that is stored in tanks at the Hanford Site. This report addresses the data analyses performed by the Rheology Working Group (RWG) and Risk Assessment Working Group. This group was composed of Pacific Northwest National Laboratory (PNNL), Bechtel National Inc. (BNI), CH2M HILL, DOE Office of River Protection (ORP), and Yasuo Onishi Consulting, LLC staff. The charter of the working group is the following:

1. To define the range of relevant waste properties that might be retrieved and handled at the Hanford Tank Farm.
2. To develop relationships that describe the solids settling and rheological behavior ranges for Hanford wastes.

The actual testing activities were performed and reported separately in referenced documentation. Because of this, many of the required topics below do not apply and are so noted.

## Test Objectives

This section is not applicable. No testing was performed for this investigation.

## Test Exceptions

This section is not applicable. No test specification as well as test exception applies to this investigation as there was no testing was performed.

## Results and Performance Against Success Criteria

This section is not applicable. No success criteria were established as there was no testing performed for this investigation.

## Quality Requirements

Since December 2001, Battelle – Pacific Northwest Division, under its use agreement with the Department of Energy (DE-AC05-76RL01831), has been providing support to BNI in accordance with the QA program approved under Subcontract No. 24590-101-TSA-W000-00004. This support has been provided under the WTP Support Project (WTPSP) QA Program and later the BNI Support Program (BNI-SP), for the technical support of the waste treatment plant being built in the 200 East area of the Hanford Site. In February 2007 the contract mechanism was switched to PNNL's Operating Contract DE-AC05-76RL01830, and the program was renamed the RPP-WTP Support Program.

The data represented in this report might refer to PNWD, PNNL, BNI-SP or WTPSP; both of these projects performed work to the same QA Program. As of February 2007, the Quality Assurance Program is described as follows:

PNNL's Quality Assurance Program is based on requirements defined in U.S. Department of Energy (DOE) Order 414.1C, Quality Assurance, and 10 CFR 830, Energy/Nuclear Safety Management, Subpart A—Quality Assurance Requirements (a.k.a. the Quality Rule). PNNL has chosen to implement the requirements of DOE Order 414.1C and 10 CFR 830, Subpart A by integrating them into the Laboratory's management systems and daily operating processes. The procedures necessary to implement the requirements are documented through PNNL's Standards-Based Management System.

PNNL implements the RPP-WTP quality requirements by performing work in accordance with the *River Protection Project – Waste Treatment Plant Support Program (RPP-WTP) Quality Assurance Plan (RPP-WTP-QA-001, QAP)*. Work will be performed to the quality requirements of NQA-1-1989 Part I, Basic and Supplementary Requirements, NQA-2a-1990, Part 2.7 and DOE/RW-0333P, Rev 13, *Quality Assurance Requirements and Descriptions (QARD)*. These quality requirements are implemented through the *River Protection Project – Waste Treatment Plant Support Program (RPP-WTP) Quality Assurance Manual (RPP-WTP-QA-003, QAM)*.

This report is based on data from testing as referenced. The PNNL assumes that the data from these references has been fully reviewed and documented in accordance with the analysts' QA Programs. PNNL only analyzed data from the referenced documentation. At PNNL, the performed calculations, the documentation and reporting of results and conclusions were performed in accordance with the *RPP-WTP Quality Assurance Manual (RPP-WTP-QA-003, QAM)*. Internal verification and validation activities were addressed by conducting an independent technical review of the final data report in accordance with PNNL procedure QA-RPP-WTP-604. This review verifies that the reported results are traceable, that inferences and conclusions are soundly based, and that the reported work satisfies the Test Specification Success Criteria. This review procedure is part of PNNL's *RPP-WTP Quality Assurance Manual*.

## Test Conditions

The scope of the RWG effort is specified in the approved WTP issue response plan (24590-WTP-PL-ENG-06-0013) and defined in subcontractor change notice (SCN) 007 and Test Specification 24590-PTF-TSP-RT-06-007, Rev 0.

Demonstrate the simulant properties used for testing *bracket expected actual waste properties*. For non-cohesive solids (Phase 1) this includes particle size, solids density, solids concentration, liquid density, and liquid viscosity. For cohesive solids (Phase 2) this includes bulk slurry density, particle size, particle density, *slurry rheology (such as consistency and yield stress) and shear strength of settled, aged sediments, as well as settled layer (heel) thickness*.

Waste received at the WTP will be subject to a feed specification supporting plant design and as agreed to in an Interface Control Document. This report compiles the existing Hanford Tank Farm rheological data addressed in italicized text above and establishes expected ranges for these properties for as-retrieved Hanford Tank Farm wastes. Various processes will be performed on these retrieved wastes which are expected to alter these property ranges from the as-retrieved conditions. Simulant development activities should focus on the expected properties of the waste streams under such processing conditions.

## Simulant Use

This section is not applicable. No testing was performed for this investigation.

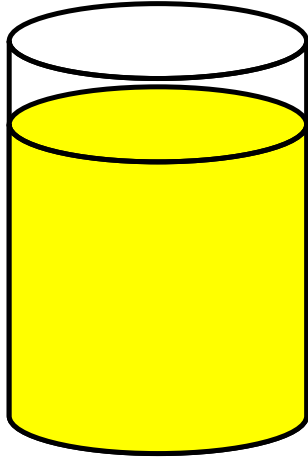
## Results of Data Analysis

The data discussed in this report can be applied to the feed systems of the WTP pretreatment facility. These data primarily consist of rheological and sedimentation data from Hanford tank farm core samples and core samples diluted with process water. An analysis of the affects of WTP process operations on these properties is not provided. Despite these limitations, three major process systems where these data apply are flow within process vessels, vertical piping, and horizontal piping. In these systems, several sludge configurations can be identified as potential operational scenarios. These scenarios and sludge configurations are shown in Figures S.1, S.2, and S.3 for process vessels (e.g. WTP EFRT issue M3), vertical piping, and horizontal piping (e.g. WTP EFRT issue M1).

Table S.1 provides a summary of the rheological parameters for each of the fluid layers shown in the associated process scenario figures. Dilution with water may result in rheological property maxima as zeta potential, particle size, and chemical composition of the solid and liquid phases change with dilution level. This table was compiled from the sections on sedimentation, shear strength, Bingham rheological parameters, and supernatant viscosity. In addition, the section discussing transient rheological modeling is summarized to provide an indication of the timescales for rheology regrowth at various process length scales. Process scales simulated include 0.1 m which is representative of process piping, 1 m represents small scale vessels, and 10 m represents large scale vessels. The timescales for each of the fluid layers to develop at each scale are shown schematically in Figure S.4. Timescales for the sediment heel to fully develop at different length scales are summarized in Table S.1.

Recovery from these slurry configurations will require the processing slurries through all of the parameters identified in Table S.1. Initially the sediment will be gelled to some extent and will possess a shear strength threshold that must be overcome. After the sediment is mobilized, the Bingham consistency and yield stress parameters will be elevated due to the large concentration of undissolved solids in the sediment bed. As mixing proceeds and supernatant liquid is blended into the sediment, the rheological properties will drop to the normal operation range when the slurry is fully suspended. This is shown graphically in Figure S.5.

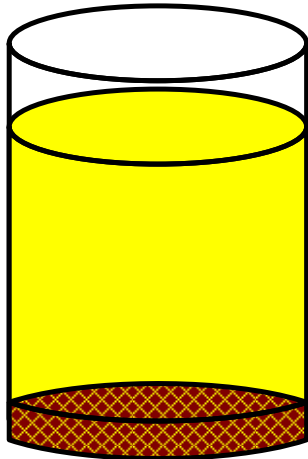
Normal operation with Newtonian fluid



Process impacts:

- cloud height
- blend times

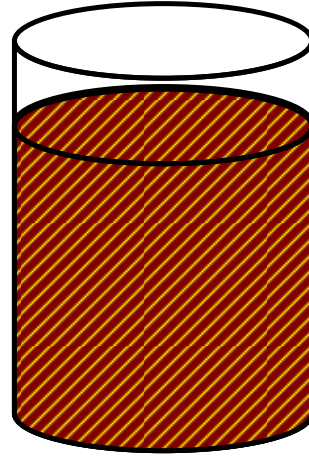
Off-normal operation with Newtonian fluid



Process impacts:

- off-bottom resuspension of solids
- blend time of solids layer

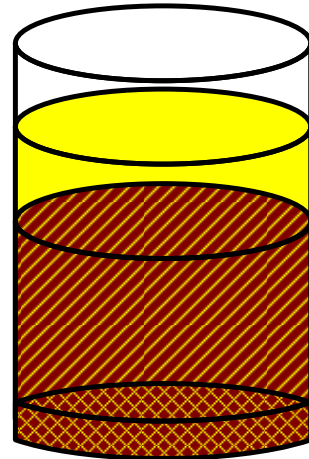
Normal operation with non-Newtonian fluid



Process impacts:

- mixing performance
- gas retention & release

Off-Normal operation with non-Newtonian fluid



Process impacts:

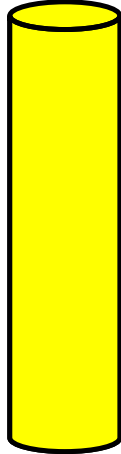
- restart of mechanical agitators/PJMs
- off-bottom resuspension of solids
- blend time liquid/solids layer
- gas retention & release

Solid – supernatant; diagonal – slurry; crosshatch – heel with coarse solids (>74  $\mu\text{m}$  & >2.7 g/cc)

**Figure S.1.** Example Operational Scenarios for Process Vessels



Normal operation with Newtonian fluid



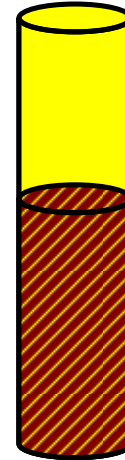
- Process impacts:
- critical flow velocity

Normal operation with non-Newtonian fluid



- Process impacts:
- flow velocity & pressure drop
  - flow regime

Off-normal operation with non-Newtonian fluid



- Process impacts:
- restart
  - flushing effectiveness

Solid – supernatant; diagonal – slurry; crosshatch – heel with coarse solids (>74 μm & >2.7 g/cc)

**Figure S.2.** Example Operational Scenarios for Vertical Process Piping

Normal operation with Newtonian fluid



- Process impacts:
- critical flow velocity

Normal operation with non-Newtonian fluid



- Process impacts:
- flow velocity and pressure drop
  - flow regime

Off-normal operation with Newtonian fluid



- Process impacts:
- restart
  - flushing effectiveness

Off-Normal operation with non-Newtonian fluid



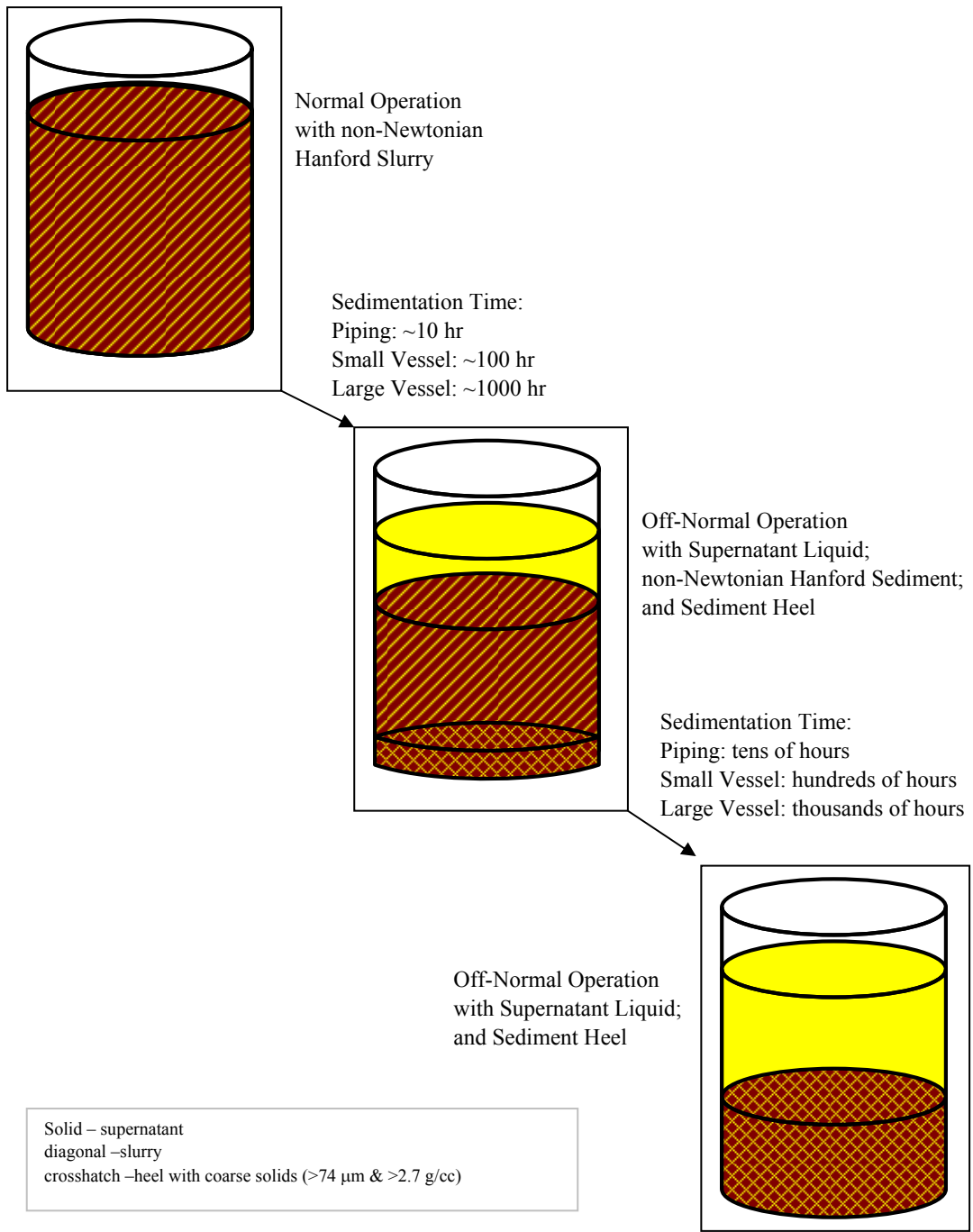
- Process impacts:
- restart
  - flushing effectiveness

Solid – supernatant; diagonal – slurry; crosshatch – heel with coarse solids (>74 μm & >2.7 g/cc)

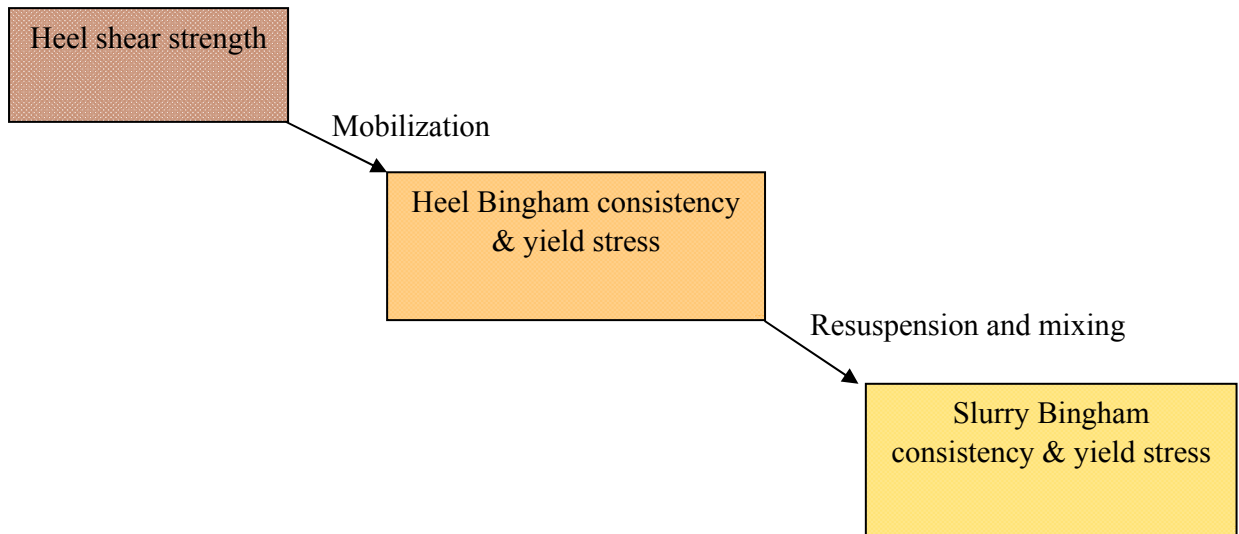
**Figure S.3.** Example Operational Scenarios for Horizontal Process Piping

**Table S.1.** Range of Rheological Parameters and Regrowth Times at Typical Process Scales

<b>Category</b>	<b>Heel Shear strength</b>	<b>Slurry/Heel Bingham Yield Stress</b>	<b>Slurry/Heel Bingham Consistency</b>	<b>Supernatant Viscosity</b>
Min <sup>(a)</sup>	40 Pa	0 Pa	1 cP	1 cP
Median <sup>(a)</sup>	700 Pa	1.5 Pa	8 cP	8 cP
Max <sup>(a)</sup>	25,000 Pa	40 Pa	110 cP	30 cP
Tank heel property after 10 hours of sedimentation in process piping (0.1 m sludge height)	25,000 Pa	40 Pa	110 cP	n/a
Tank heel property after 100 hours of sedimentation in a medium-scale vessel (1 m sludge height)	25,000 Pa	40 Pa	110 cP	n/a
Tank heel property after 1000 hours of sedimentation in a large-scale vessel (10 m sludge height)	25,000 Pa	40 Pa	110 cP	n/a
(a) Statistics performed on all compiled data discussed in this report. n/a – not applicable.				



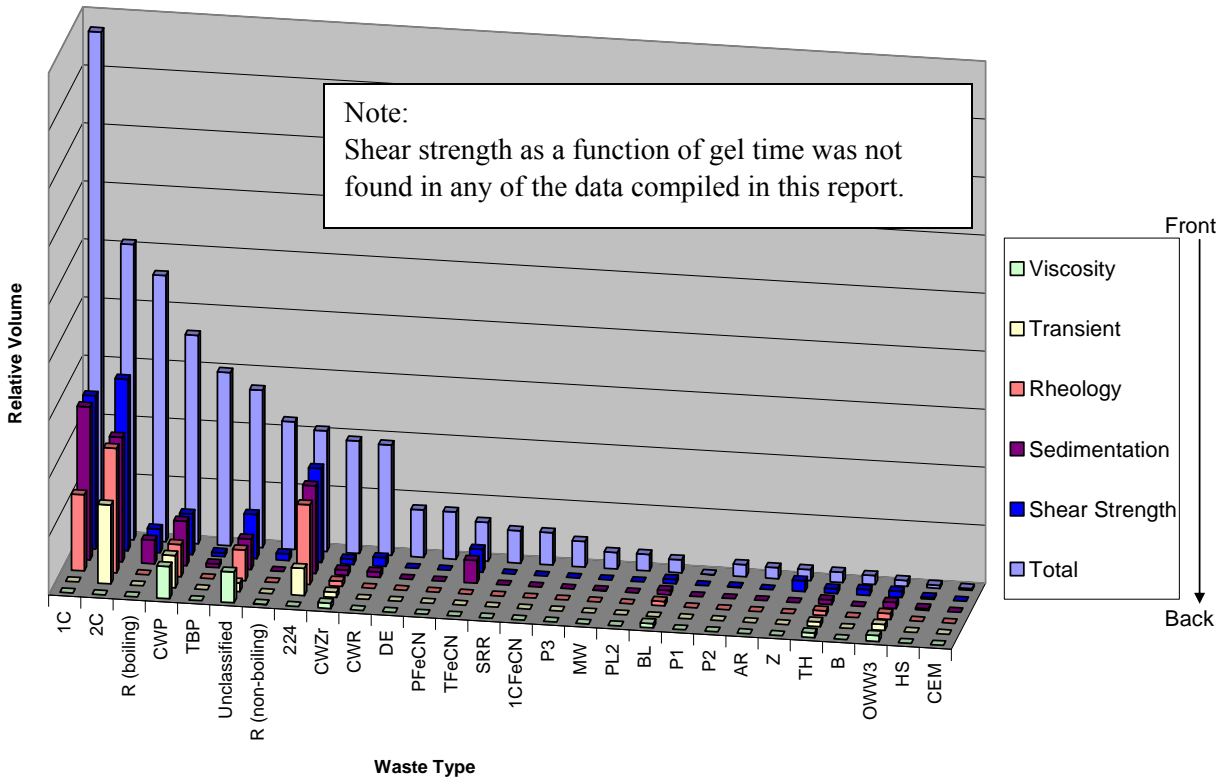
**Figure S.4.** Illustration of Development of Sludge Process Heel and Fully Settled Configuration at Various Process Scales



**Figure S.5.** Rheological Properties Encountered During Recovery from Process Upset Conditions

## Discrepancies and Follow-on Tests

Rheology data and associated physical properties for Hanford tank wastes were compiled from all the readily available reports, but many gaps were observed when analyzing the data. These data include in situ as well as laboratory analysis of samples removed from the tanks. The gaps in the waste types analyzed are reported in each section of the report. Figure S.6 provides a summary of these gaps. The relative volume of wastes modeled for liquid viscosity, sedimentation, shear strength, rheological parameters (Bingham plastic model), and rheological parameters as a function of settling are plotted as a function of waste type. Additional testing of archive samples or samples being gathered on wastes that were collected as part of the analysis of the M-12 samples would fill in many of the gaps from current rheological and physical properties data.



**Figure S.6.** Relative Volume of Waste Types Modeled Based on Waste Tank Data Available for Liquid Viscosity, Sedimentation, Shear Strength, Rheology, and Transient Modeling Compared with the Total Volume of Each Sludge Waste Type

## References

Bechtel National, Inc. 2006. *Issue Response Plan for Implementation of External Flowsheet Review Team (EFRT) Recommendations - M3, Inadequate Mixing System Design*. 24590-WTP-PL-ENG-06-0013 Rev 000, Bechtel National, Inc., Richland, Washington.

Bechtel National, Inc. 2006. *Scaled Testing to Determine the Adequacy of the WTP Pulse Jet Mixer Designs*. 24590-PTF-TSP-RT-06-007 Rev 0, Bechtel National, Inc., Richland, Washington.

WTP/RPP-MOA-BNI-00007, Subcontractor Change Notice No. 007.



## Acronyms and Abbreviations

BBI	Best Basis Inventory
BNI	Bechtel National, Inc.
DOE	U.S. Department of Energy
ESP	Environmental Simulation Program
HLW	High Level Waste
PJM	Pulse Jet Mixer
PNNL	Pacific Northwest National Laboratory
QA	Quality Assurance
RPP	River Protection Project
TWINS	Tank Waste Information System
WTP	Waste Treatment Plant





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# 1.0 Introduction

The U.S. Department of Energy (DOE) Office of River Protection Waste Treatment and Immobilization Plant (WTP) is being designed and built to pretreat and then vitrify a large portion of the wastes in Hanford's 177 underground waste storage tanks. Once the material is transferred from the underground waste storage tanks to the WTP, the mixing systems at WTP must be capable of blending liquids, maintaining solids suspended, and resuspending settled solids.

In vessels where process streams are mixed, the liquids are blended to the degree required for processing and sampling. The pulse jet mixer (PJM) mixing test performance criteria require that all points in the vessel must be reached during blending to ensure that there will be no zones where the material is not blended, and the slurry being blended into the vessel must achieve a sufficiently uniform vessel concentration.

The WTP PJM-mixed vessels do not have restrictive criteria on the degree of uniformity of solids concentration within the vessel liquid. However, the mixing must be sufficient to maintain the solids in suspension so that they do not accumulate on the bottom and can be transferred through the pump suction line. Solids suspended from the bottom of the vessel must be sufficiently lifted in a repeatable pattern so that they can be carried with the flowing fluid into the vessel suction line.

Mixing of tank waste slurries is also required for hydrogen control. During normal operations the vessels may be mixed intermittently, but must be mixed with a frequency to ensure that the hydrogen inventory is controlled. After a design basis event the important-to-safety air supply is limited and the PJMs will be operated intermittently. Between operating periods, solids will form a settled layer, which may have cohesive properties. The PJMs must be able to cause motion of the accumulated solids layer adequate to release hydrogen. Rheological properties of the suspending medium, solids suspensions, and settled solids are included in the parameters that define the ability of the PJM to blend, maintain solids suspensions, and resuspend settled solids.

Accurate rheological data of Hanford tank wastes at varying conditions including as a function of sedimentation are critical in validating the performance of the WTP-PJM mixing systems. This report provides a compilation of the available rheological data for Hanford tank wastes and empirical models describing this data. Rheological properties were modeled as a function of physical properties (volume percent settled solids, sedimentation rate, etc.) to provide a predictive tool for rheological behavior for different waste types under differing conditions.

This report presents the data sources considered and the development of the best-estimate data sets for rheological properties. The relation of the available data sets with regard to the insoluble solid inventory at Hanford is discussed. Quantifiable uncertainties in the data are elucidated. Liquid viscosity, sedimentation, and rheological models are also presented. Conclusions and recommendations are presented based on the models and data available.

## 2.0 Quality Requirements

Since December 2001, Battelle – Pacific Northwest Division, utilizing its use agreement with the Department of Energy (DE-AC05-76RL01831), has been providing support to Bechtel National, Inc. (BNI) in accordance with the Quality Assurance (QA) program approved under Subcontract No. 24590-101-TSA-W000-00004. This support has been provided under the WTP Support Project (WTPSP) QA Program and later the BNI Support Program (BNI-SP) for the technical support of the waste treatment plant being built in the 200 East area of the Hanford Site. In February 2007, the contract mechanism was switched to Pacific Northwest National Laboratory (PNNL) Operating Contract, DE-AC05-76RL01830, and the program was renamed the RPP-WTP Support Program.

The data represented in this report might refer to PNWD, PNNL, BNI-SP or WTPSP; both of these projects performed work to the same QA Program. As of February 2007, the Quality Assurance Program is described as follows:

PNNL's Quality Assurance Program is based on requirements defined in U.S. Department of Energy (DOE) Order 414.1C, Quality Assurance, and 10 CFR 830, Energy/Nuclear Safety Management, Subpart A–Quality Assurance Requirements (a.k.a. the Quality Rule). PNNL has chosen to implement the requirements of DOE Order 414.1C and 10 CFR 830, Subpart A by integrating them into the Laboratory's management systems and daily operating processes. The procedures necessary to implement the requirements are documented through PNNL's Standards-Based Management System.

PNNL implements the RPP-WTP quality requirements by performing work in accordance with the *River Protection Project – Waste Treatment Plant Support Program (RPP-WTP) Quality Assurance Plan (RPP-WTP-QA-001, QAP)*. Work will be performed to the quality requirements of NQA-1-1989 Part I, Basic and Supplementary Requirements, NQA-2a-1990, Part 2.7 and DOE/RW-0333P, Rev 13, *Quality Assurance Requirements and Descriptions (QARD)*. These quality requirements are implemented through the *River Protection Project – Waste Treatment Plant Support Program (RPP-WTP) Quality Assurance Manual (RPP-WTP-QA-003, QAM)*.

This report is based on data from testing as referenced. The PNNL assumes that the data from these references has been fully reviewed and documented in accordance with the analysts' QA Programs. PNNL only analyzed data from the referenced documentation. At PNNL, the performed calculations, the documentation and reporting of results and conclusions were performed in accordance with the *RPP-WTP Quality Assurance Manual (RPP-WTP-QA-003, QAM)*. Internal verification and validation activities were addressed by conducting an independent technical review of the final data report in accordance with PNNL procedure QA-RPP-WTP-604. This review verifies that the reported results are traceable, that inferences and conclusions are soundly based, and that the reported work satisfies the Test Specification Success Criteria. This review procedure is part of PNNL's *RPP-WTP Quality Assurance Manual*.

### 3.0 Hanford Tank Waste

Radioactive waste from the reprocessing of spent nuclear fuel on the Hanford Site was transferred to underground storage tanks. Four different chemical processes were used for reprocessing this spent nuclear fuel, and waste from each of these processes exists in these 177 underground storage tanks. The four processes used were the bismuth phosphate (BiPO<sub>4</sub>) process, the tributyl phosphate (TBP) process, the reduction-oxidation (REDOX) process, and the plutonium-uranium extraction (PUREX) process. Wastes with different chemical composition and properties were generated in multiple steps of these processes, and modifications to the processes have resulted in multiple waste types. Some of this waste was treated in the underground storage tanks, resulting in additional waste types. Each waste type was made alkaline for storage in the steel tanks. Table 3.1 lists the waste type, acronym, and a brief description of each waste type. The definitions were adapted from Meacham (2003).

**Table 3.1.** List of Waste Type Definitions

Waste Type	Definition
1C	BiPO <sub>4</sub> first cycle decontamination waste (1944-1956)
1CFeCN	Ferrocyanide sludge from in-farm scavenging of 1C supernatants in TY-Farm (1955-1958)
224	lanthanum fluoride process "224 Building" waste (1952-1956)
2C	BiPO <sub>4</sub> second cycle decontamination waste (1944-1956)
A1-SltCk	Saltcake from the first 242-A Evaporator campaign (1977-1980)
A2-SltSlr	saltcake from the second 242-A Evaporator campaign (1981-1994).
AR	Washed Plutonium-Uranium Extraction (PUREX) sludge (1967-1976)
B	high-level acid waste from PUREX processed at B Plant for Sr recovery (1967-1972)
BL	low-level waste from B Plant Sr and Cs recovery operations (1967-1976)
CEM	Portland Cement
CSR	Cesium recovery, supernatant from which Cs has been removed
CWP	PUREX cladding waste (1956-1960 and 1961-1972)
CWR	REDOX cladding waste, aluminum clad fuel (1952-1960 and 1961-1972)
CWZr	zirconium cladding waste (PUREX and REDOX)
DE	diatomaceous earth
HS	hot semi-works <sup>90</sup> Sr recovery waste (1962-1967)
MW	BiPO <sub>4</sub> process metal waste (1944-1956)
OWW3	PUREX organic wash waste (1968-1972)
P1	PUREX HLW (1956-1962)
P2	PUREX HLW (1963-1967)
P3	PUREX HLW (1983-1988)
PFeCN	Ferrocyanide sludge from in-plant scavenged supernatant (1954-1958)
PL2	PUREX low-level waste (1983-1988)
R (boiling)	boiling REDOX HLW (1952-1966)
R (non-boiling)	non-boiling REDOX HLW (1952-1966)
R-SltCk	Saltcake from self-concentration in S- and SX-Farms (1952-1966)
S1-SltCk	Saltcake from the first 242-S Evaporator campaign using 241-S-102 feed tank (1973-1976)
S2-SltSlr	Saltcake from the second 242-S Evaporator campaign using 241-S-102 feed tank (1976-1980)
SRR	HLW transfers (late B Plant operations)
T2-SltCk	Saltcake from the second 242-T Evaporator campaign using 241-TX-118 feed tank (1965-1976)
TBP	tributyl phosphate waste (from solvent based uranium recovery operations)
TFeCN	ferrocyanide sludge produced by in-tank or in-farm scavenging
TH	PUREX waste from processing of thoria targets
Z	Z Plant waste



Rheological data is available on 40 tanks that contain several different waste types. The primary and secondary waste types for the solids in these 40 tanks, as described in the Tank Waste Information System (TWINS) database, are listed in Table 3.2. The waste types for the liquids in these tanks are listed in Table 3.3. Rheological measurements have been made on samples from the tanks that are listed in these tables, but the data have not been published or the published documents are not currently accessible. Additional effort will be needed to obtain and analyze the rheological data from these tanks.

**Table 3.2.** Primary and Secondary Waste Types for the Solids in Tanks with Rheological Data Available

Tank	Primary Waste Type	Secondary Waste Type
A-101	A1-SltCk	P2
AN-102	A2-SltSlr	--
AN-103	A2-SltSlr	--
AN-104	A2-SltSlr	--
AN-105	A2-SltSlr	--
AN-107	A2-SltSlr	--
AP-104	No Insoluble Solids	
AW-101	A2-SltSlr	--
AW-103	CWZr	--
AY-101	NA <sup>(a)</sup>	--
AY-102	NA <sup>(a)</sup>	BL
AZ-101	P3	NA <sup>(a)</sup>
AZ-102	P3	PL2, SRR
B-111	2C	P2, B
B-201	224	--
B-202	224	--
B-203	224	--
BX-107	1C	--
C-103	CWP	--
C-104	CWP	CWZr, OWW3, TH
C-106	NA <sup>(a)</sup>	--
C-107	1C	CWP, SRR
C-109	TFeCN	CWP, 1C, HS
C-110	1C	--
C-112	TFeCN	1C, CWP, HS
S-102	NA SltCk <sup>(b)</sup>	R (non-boiling)
S-104	R (boiling)	CWR
S-112	S1-SltCk	R (non-boiling)
SY-101	S2-SltSlr	--
SY-102	NA <sup>(a)</sup>	Z
SY-103	S2-SltSlr	--
T-102	CWP	MW
T-104	1C	--
T-107	1C	CWP, TBP
T-110	2C	224
T-111	224	2C
T-203	224	--
T-204	224	--
U-103	S1-SltCk	S2-SltSlr, R (non-boiling)
U-107	S2-SltSlr	CWR, T2-SltCk
(a) Waste volume information indicates that this waste type is unclassified solid sludge.		
(b) Waste volume information indicates that this waste type is unclassified saltcake.		

**Table 3.3.** Primary and Secondary Waste Types for Liquids in Tanks with Rheological Data Available

Tank	Primary Waste Type	Secondary Waste Type
A-101 (interstitial only)	A1-SltCk	--
AN-102	NA <sup>(a)</sup>	--
AN-103	A2-SltSlr	--
AN-104	A2-SltSlr	--
AN-105	A2-SltSlr	--
AN-107	A2-SltSlr	--
AP-104	NA <sup>(a)</sup>	--
AW-101	A2-SltSlr	--
AW-103	NA <sup>(a)</sup>	A1-SltCk (interstitial)
AY-101	NA <sup>(a)</sup>	--
AY-102	NA <sup>(a)</sup>	BL (interstitial)
AZ-101	P3	--
AZ-102	P3	--
B-111	CSR	--
B-201	No Free Liquid	
B-202	No Free Liquid	
B-203	NA <sup>(a)</sup>	--
BX-107	No Free Liquid	
C-103	NA <sup>(a)</sup>	--
C-104	No Free Liquid	
C-106	NA <sup>(a)</sup>	--
C-107	No Free Liquid	
C-109	No Free Liquid	
C-110	1C	--
C-112	No Free Liquid	
S-102	No Free Liquid	
S-104 (interstitial only)	R-SltCk	--
S-112	No Free Liquid	
SY-101	S2-SltSlr	--
SY-102	NA <sup>(a)</sup>	Z (interstitial only)
SY-103	S2-SltSlr	--
T-102	CSR	--
T-104	No Free Liquid	
T-107	No Free Liquid	
T-110	2C	--
T-111	No Free Liquid	
T-203	No Free Liquid	
T-204	No Free Liquid	
U-103	S1-SltCk	--
U-107 (interstitial only)	S2-SltSlr	T2-SltCk
(a) Waste volume information indicates that this waste type is unclassified liquid.		

Waste type definitions have evolved over time as additional information on the composition of wastes transferred to the Hanford tanks has been identified. The latest modifications were included in Revision 5

of the Hanford Defined Waste (HDW) Model, which was published in February 2004 (Higley 2004). Most of these changes are included in the 2006 Best Basis Inventory (BBI), which is the database provided in TWINS and used in this report for determining the sludge volumes associated with each waste type. In the 2006 BBI, waste types 1C1 and 1C2 are combined as 1C, and waste types 2C1 and 2C2 are combined as 2C.

The 2002 BBI is used in the current Environmental Simulation Program (ESP)<sup>(a)</sup> model; therefore, some of the wastes types in the 2006 BBI were combined to be consistent with the ESP model and previous reports. Waste types identified in the 2006 BBI are compared with the waste types used in this report in Table 3.4. A few sludge, saltcake, and liquid layers in Hanford tanks have not been identified as a particular waste type and are listed as unclassified. The acronym NA is used for these unclassified wastes in the BBI presented in TWINS.

Twenty-nine of the 41 waste types described in Meacham (2003) are included in the tanks identified as having rheological data. Diatomaceous earth is included as a waste type in BBI but is not included in Meacham (2003); therefore, the total number of waste types is 42. Also included in TWINS are waste transfers and unclassified waste types. Only 26 of the 42 waste types are listed as sludge in TWINS, and these waste types are the focus of this study. Other waste types with rheological data are included in the data set to provide additional supporting data. Seven of the 26 sludge waste types are not represented in the rheology data set. These include 1CFeCN, AR, DE, P1, PFeCN, CEM, and Z. Waste transfers are also not represented in the rheological data. The definitions of these waste types are included in Table 3.1 and listed in Table 3.4.

REDOX high-level wastes (HLW) are classified as R1 and R2 in the 2006 BBI based on the date of waste generation, but these classifications do not indicate the thermal history of the REDOX waste, which is essential in determining whether gibbsite or boehmite is the predominant aluminum species in the waste. Therefore, REDOX HLW were reclassified as REDOX boiling and REDOX non-boiling waste types to provide waste type definitions that segregated the aluminum-containing sludges based on the predominant aluminum phase (gibbsite or boehmite). This reclassification was based on thermal history and aluminum leaching factors in these wastes, as described in Meacham (2003).

The 224 waste is currently in the Hanford baseline to be dried and transported to the Waste Isolation Pilot Plant (WIPP) as transuranic (TRU) waste. The inclusion of the 224 waste in this report raises the overall significance of the rheology characterization of the Hanford sludge. While this waste might not be a direct feed to WTP, it may be representative of sludge in other tanks that may be a feed to WTP. For example, Tanks T-110, T-111, and T-112 contain a blend of 224 and 2C waste that may not meet TRU waste specifications.

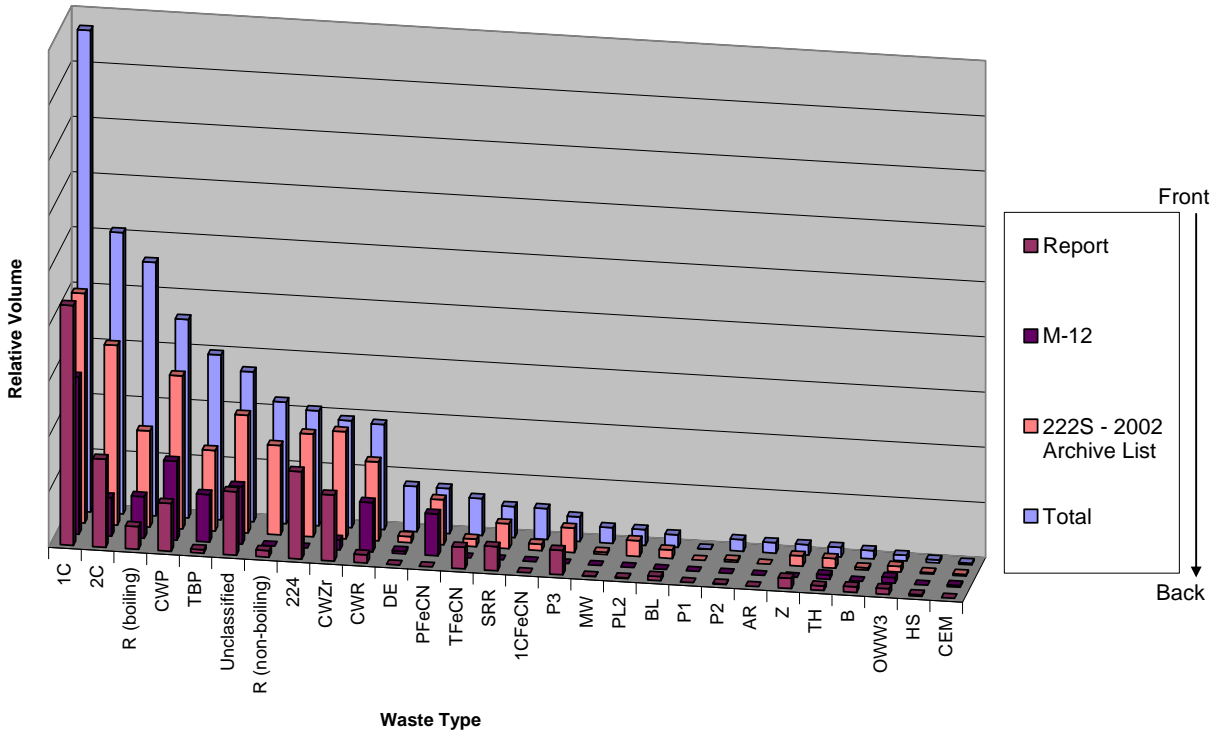
Rheology data available from tank waste core samples and falling ball rheometry are plotted as a function of waste type in Figure 3.1. The volume of waste in each tank for each waste type was determined using the TWINS database. Additional rheology data are being gathered on wastes that were collected as part of the analysis of the M-12 samples. The increase in the amount of rheology data that will be available based on these analyses is also shown in Figure 3.1.

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(a) ESP was supplied and developed by OLI Systems, Inc., Morris Plains, New Jersey.

**Table 3.4.** Comparison of Waste Type Groups

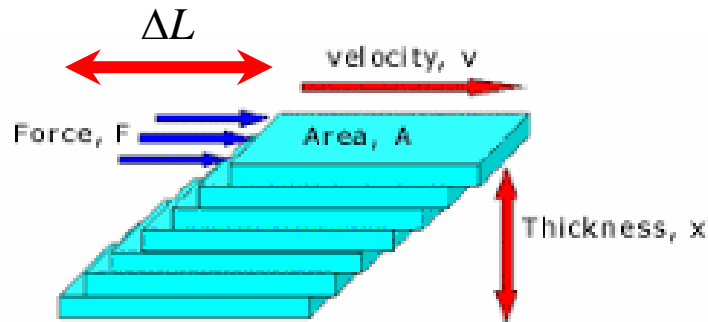
<b>2006 BBI</b>	<b>This Report</b>
<i>Bismuth Phosphate Process Waste Types</i>	
MW1	MW
MW2	
1C	1C
2C	2C
224-1	224
224-2	
<i>Uranium Recovery and Scavenging Waste Types</i>	
1CFeCN	1CFeCN
PFeCN	PFeCN
TBP	TBP
TFeCN	TFeCN
<i>REDOX Process Waste Types</i>	
R1	R (boiling) or R (non-boiling)
R2	
CWR1	CWR
CWR2	
<i>PUREX Process Waste Types</i>	
P1	P1
P2	P2
P3AZ1	P3
P3AZ2	
CWP1	CWP
CWP2	
CWZr1	CWZr
CWZr2	
OWW3	OWW3
PL2	PL2
TH1	TH
TH2	
<i>Cesium and Strontium Recovery Waste Types</i>	
HS	HS
AR	AR
B	B
BL	BL
CSR	CSR
SRR	SRR
<i>Saltcake and Salt Slurries Waste Types</i>	
A1-SltCk	A1-SltCk
A2-SltSlr	A2-SltSlr
R-SltCk	R-SltCk
S1-SltCk	S1-SltCk
S2-SltSlr	S2-SltSlr
T2-SltCk	T2-SltCk
<i>Other Process Facility Wastes</i>	
Z	Z
<i>Miscellaneous Wastes</i>	
CEM	Portland Cement
DE	DE



**Figure 3.1.** Gaps in Rheology Data Available for Sludges in the Entire Hanford Tank Waste Inventory as a Function of Waste Type

## 4.0 Rheology Theory

Rheology is the study of the flow and deformation of materials. When a force (i.e., stress) is placed on an object, the object deforms or strains. Many relationships have been found relating stress to strain for various fluids. Flow behavior of a fluid can generally be explained by considering a fluid placed between two plates of thickness  $x$  (Figure 4.1). The lower plate is held stationary while a force,  $F$ , is applied to the upper plate of area,  $A$ , that results in the plating moving at velocity,  $v$ . If the plate moves a length,  $\Delta L$ , the strain,  $\gamma$ , on the fluid can be defined by Eq. (4.1).



**Figure 4.1.** Diagram of Fluid Flow Between Stationary and Moving Plates

$$\gamma = \frac{\Delta L}{x} \quad (4.1)$$

The rate of change of strain (also called shear rate),  $\dot{\gamma}$ , can be defined by Eq. (4.2). Because the shear rate is defined as the ratio of a velocity to a length, the units of the variable are the inverse of time, typically  $s^{-1}$ .

$$\dot{\gamma} = \frac{d\gamma}{dt} = \frac{d}{dt} \left( \frac{\Delta L}{x} \right) = \frac{v}{x} \quad (4.2)$$

Typical shear rates of food-processing applications can be seen in Table 4.1. Depending on the application, shear rates in the range of  $10^{-6}$  to  $10^7 s^{-1}$  are possible. Human perception of a fluid is typically based on a shear rate of approximately  $60 s^{-1}$ .

The shear stress applied to the fluid can be found by Eq. (4.3). Because the shear stress is defined as the ratio of a force to an area, the units of the variable are pressures, typically expressed in Pa ( $N/m^2$ ).

$$\tau = \frac{F}{A} \quad (4.3)$$

**Table 4.1.** Typical Shear Rates in Food-Processing Applications

Situation	Shear Rate Range (1/s)	Typical Applications
Sedimentation of particles in a suspending liquid	$10^{-6} - 10^{-3}$	Medicines, paints, spices in salad dressing
Leveling due to surface tension	$10^{-2} - 10^{-1}$	Frosting, Paints, printing inks
Draining under gravity	$10^{-1} - 10^1$	Vats, small food containers
Extrusion	$10^0 - 10^3$	Snack and pet foods, toothpaste, cereals, pasta, polymers
Calendering	$10^1 - 10^2$	Dough sheeting
Pouring from a bottle	$10^1 - 10^2$	Foods, cosmetics, toiletries
Chewing and swallowing	$10^1 - 10^2$	Foods
Dip coating	$10^1 - 10^2$	Paints, confectionery
Mixing and stirring	$10^1 - 10^3$	Food processing
Pipe flow	$10^0 - 10^3$	Food processing, blood flow
Rubbing	$10^2 - 10^4$	Topical application of creams and lotions
Brushing	$10^3 - 10^4$	Brush painting, lipstick, nail polish
Spraying	$10^3 - 10^5$	Spray drying, spray painting, fuel atomization
High-speed coating	$10^4 - 10^6$	Paper
Lubrication	$10^3 - 10^7$	Bearings, gasoline engines

The apparent viscosity of the fluid is defined as the ratio of the shear stress to shear rate (see Eq. 4.4). Often the shear stress and viscosity vary as a function of shear rate. Since the viscosity is defined as the ratio of shear stress to shear rate, the units of the variable are Pa•s. Typically, viscosity is reported in units of centipoise (cP; where 1 cP = 1 mPa•s).

$$\eta(\dot{\gamma}) = \frac{\tau(\dot{\gamma})}{\dot{\gamma}} \quad (4.4)$$

For Newtonian fluids, the apparent viscosity is independent of shear rate (Eq. 4.5). Examples of the viscosity of common Newtonian materials can be seen in Table 4.2.

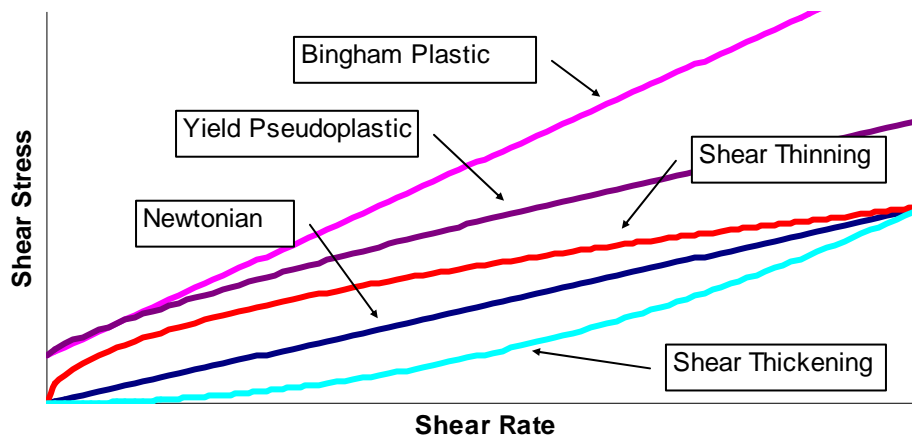
$$\tau = \eta\dot{\gamma} \quad (4.5)$$

where  $\tau$  is the shear stress,  $\eta$  is the Newtonian viscosity, and  $\dot{\gamma}$  is the shear rate.

Fluids that do not behave as Newtonian fluids are referred to as non-Newtonian fluids. Rheograms or plots of shear stress versus shear rate are typically used to characterize non-Newtonian fluids. Examples of typical rheograms can be seen in Figure 4.2.

**Table 4.2.** Viscosities of Several Common Newtonian Fluids

Material	Viscosity at 20°C (cP)
Acetone	0.32
Water	1.0
Ethanol	1.2
Mercury	1.6
Ethylene Glycol	20
Corn Oil	71
Glycerin	1,500



**Figure 4.2.** Rheograms of Various Fluid Types

Shear-thinning and shear-thickening fluids can be modeled by the Ostwald equation (Eq. 4.6). If  $n < 1$ , then the material is referred to as pseudoplastic (shear thinning). If  $n > 1$ , then that material is referred to as dilatant (shear thickening). These fluids exhibit decreasing or increasing apparent viscosities as shear rate increases, depending on whether the fluid is shear thinning or shear thickening, respectively. Since shear-thickening flow behavior is rare, shear-thickening behavior is often an indication of possible secondary flow patterns or other measurement errors.

$$\tau = m\dot{\gamma}^n \quad (4.6)$$

where

$m$  = the power law consistency coefficient

$n$  = the power law exponent

$\dot{\gamma}$  = is the shear rate.

A rheogram for a Bingham plastic does not pass through the origin. When a rheogram possesses a non-zero y-intercept, the fluid is said to possess a yield stress. A yield stress is a shear-stress threshold that defines the boundary between solid-like behavior and fluid-like behavior. The fluid will not begin to flow



until the yield stress threshold is exceeded. For Bingham plastic materials, once enough force has been applied to exceed the yield stress, the material approaches Newtonian behavior at high shear rates (Eq. 4.7).

$$\tau = \tau_B + \eta_p \dot{\gamma} \quad (4.7)$$

where  $\tau_B$  is the Bingham yield stress,  $\eta_p$  is the plastic viscosity, and  $\dot{\gamma}$  is the shear rate.

Fluids that exhibit a non-linear rheogram with a yield stress are typically modeled by the three-parameter Herschel-Bulkley equation (Eq. 4.8). Again, shear-thickening behavior is uncommon, and typically the Herschel-Bulkley power-law exponent is less than unity.

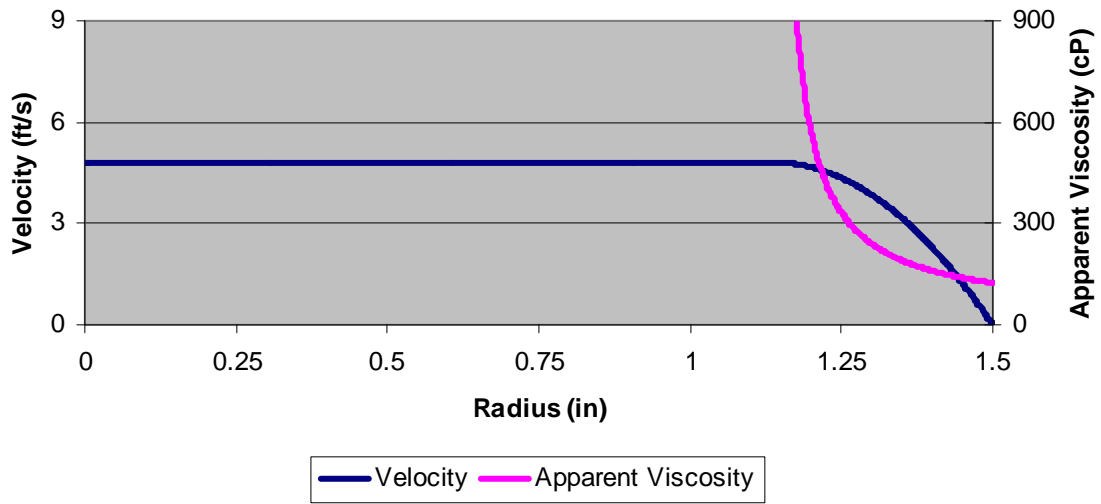
$$\tau = \tau_H + k\dot{\gamma}^b \quad (4.8)$$

where

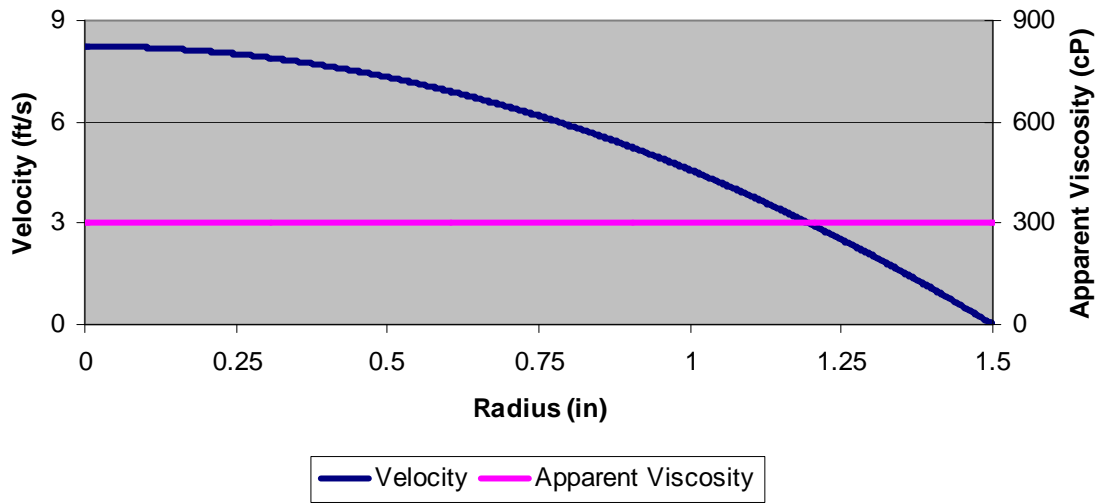
- $\tau_H$  = yield stress
- k = Herschel-Bulkley consistency coefficient
- b = Herschel-Bulkley power law exponent
- $\dot{\gamma}$  = shear rate.

An example of these rheological properties can be considered through a pipeline flow scenario through a 3-inch ID smooth pipe transporting 90 gallons per minute of fluid. This equates to an average pipeline velocity of 4.1 ft/sec. The fluid is a Bingham plastic with a Bingham yield stress,  $\tau_B$ , of 30 Pa, a Bingham consistency or plastic viscosity,  $\eta_p$ , of 30 cP, and a slurry density of 1.2 kg/L. In this case, the fluid flow will be in the laminar regime with the velocity and apparent viscosity profiles shown in Figure 4.3. The flow profile reflects a “plug flow” regime where the center core of the fluid moves at constant velocity. This because the shear stress in this region does not exceed the yield stress of the fluid and acts as a solid material with an infinite apparent viscosity. At a radius of approximately 1.1 inches, the shear stress in the pipe exceeds the yield stress of the fluid and the fluid transitions from behaving as a solid to behaving as a “shear thinning” liquid. The apparent viscosity in the sheared region near the pipe wall (1.1–1.5 inch radius) drops from an infinite value to approximately 100 cP at the pipe wall. Pressure drop for flow under these conditions is calculated at 9 psig/100 ft of straight horizontal pipe.

The case of a Newtonian fluid with the same pressure drop is then considered. At 90 gpm, a Newtonian viscosity of 300 cP is required for a 9 psi/100 ft pressure drop. The flow profiles for this system are shown in Figure 4.4. The flow profile shows a parabolic velocity profile that is characteristic of Newtonian, laminar pipe flows. The apparent viscosity in this case is constant at 300 cP throughout the pipe radius.



**Figure 4.3.** Example Flow Profiles for a Bingham Plastic Fluid (30 cP consistency, 30 Pa yield stress) in a 3-inch-ID Smooth Pipe at 90 gpm



**Figure 4.4.** Example Flow Profiles for a Newtonian Fluid (30 cP viscosity) in a 3-inch-ID Smooth Pipe at 90 gpm

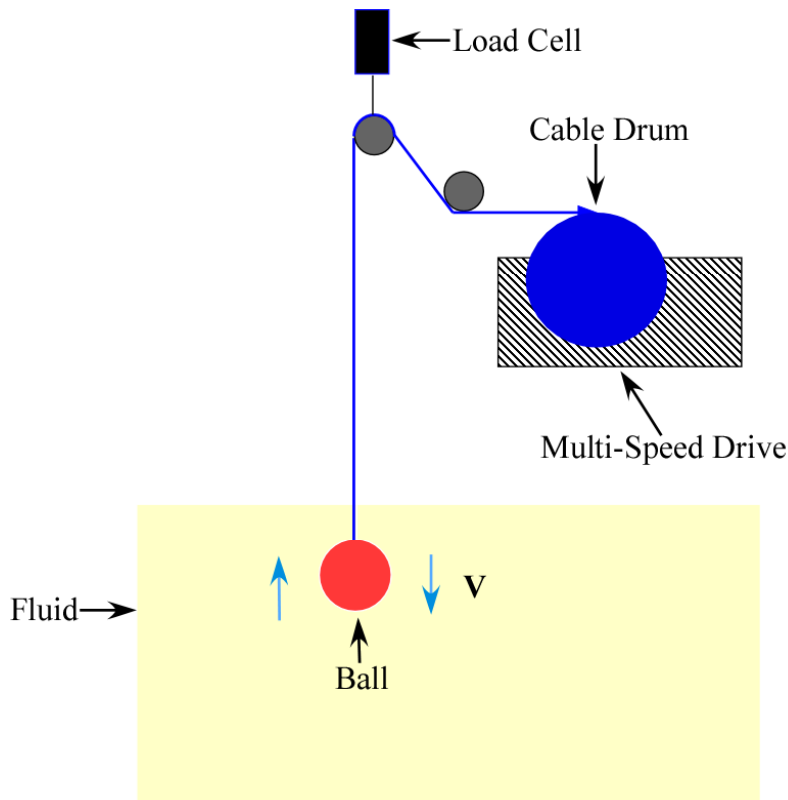
## 5.0 Rheology Measurements

Colloidal suspensions such as tank wastes exhibit a wide range of rheological behavior; therefore, rheological measurement of tank wastes requires a wide range of capabilities. Measurements of rheological properties of actual Hanford tank wastes have been performed in-situ using a falling ball rheometer and on core samples removed from the tanks using viscometers or rheometers. Rheological properties have also been calculated from extrusion data of tank waste core samples (slump tests).

### 5.1 Falling Ball Rheometer (In Situ Rheology)

The falling ball rheometer measures the drag force on a ball of known mass as it moves through the waste at various speeds from which rheology and density of the waste can be estimated. Physical models that form relationships are used to transform the drag force and velocity of the ball into fluid properties (density, viscosity, and yield strength). Different fluid types (Newtonian, Bingham plastic, or power law fluids) require different relationships. Details of the data reduction methodology are reported by Shephard et al. (1994).

The falling ball rheometer consists of a 71-N (16-lb), 9.12-cm diameter tungsten alloy ball tethered to a steel cable that is let out and retrieved from a spool at precise speeds using a computer-controlled drive system. A load cell measures the tension on the cable. A schematic of the system is shown in Figure 5.1.



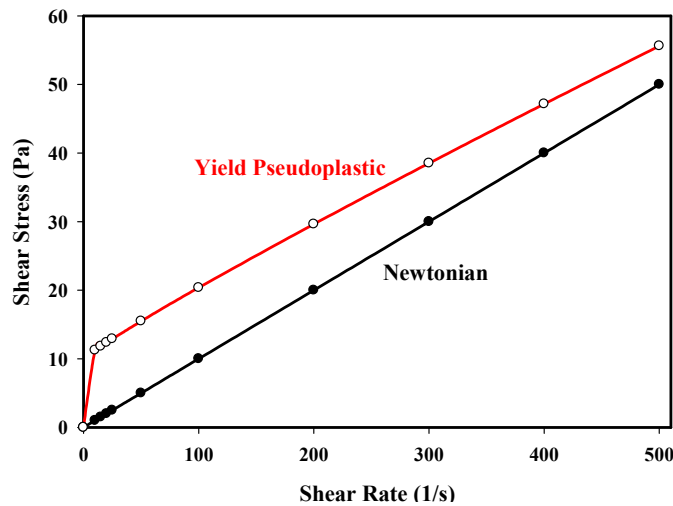
**Figure 5.1.** Schematic of the Falling Ball Rheometer

## 5.2 Laboratory Rheology Measurements

The majority of the rheology data are obtained from measurements of samples removed from the Hanford tanks. These samples included push- and rotary-mode core samples, auger samples, and grab samples. Rheological properties of these samples were obtained using rheometers under varying conditions depending upon the viscosity of the sample. The measuring system of a rheometer consists of a fixed part and a rotating part. Rheological properties obtained by laboratory measurements include viscosity, yield stress, and shear strength. Viscosity and yield stress are determined from a plot of shear stress as a function of shear rate. Shear strength is obtained from measuring shear stress as a function of time at a low shear rate that is held constant.

### 5.2.1 Viscosity and Yield Stress

Viscosity and yield stress (also call yield strength) are measured by plotting shear stress as a function of shear rate (rheogram). An example of a typical rheogram is provided in Figure 5.2. Most of the rheograms for Hanford tank waste samples include a curve with increasing shear rate and a second curve with decreasing shear rate. Generally, some thixotropic behavior (i.e., time dependency and hysteresis) is observed in these two curves.



**Figure 5.2.** Rheogram of a Newtonian and Yield Pseudoplastic Fluid

Some rheometers measure shear stress as a function of shear rate (controlled-rate rheometers), while others measure shear rate as a function of shear stress (controlled-stress rheometers). Both types of systems were used to generate the data used in this report. Fixed and rotating parts of the rheometer varying according to the rheometer design and the viscosity of the sample. Both cone and plate and concentric cylinder geometries were used to measure tank waste samples. Rheograms were obtained at multiple temperatures and dilution levels (solids content) for many of the tank waste samples. Calibration of the systems was checked with Newtonian fluid standards of known viscosity.

Empirical curve fits of the data in the rheograms were performed using well-accepted models. Four different models were used in these analyses. These models included Newtonian, Bingham Plastic, Power Law, and Herschel-Bulkley fits described in Section 4. Additional parameters are included in each of these successive curve fits to provide a better fit of the data. The mathematical equations for these curve fits are provided in Eq. (4.5) through (4.8).

Equation (4.5) is the Newtonian model. No yield stress is observed in Newtonian fluids, and viscosity is constant over the entire shear rate range. In this equation the slope of the line is the Newtonian viscosity.

Equation (4.7) is the Bingham plastic model where the fluid has a positive yield stress as indicated by a non-zero intercept with the ordinate (y-axis) followed by a linear increase in the shear stress as function of shear rate. The slope of this line is the Bingham viscosity. The difference between a Bingham plastic and a Newtonian fluid is the presence of a non-zero yield stress.

Equation (4.6) is the power law model (sometimes called the Ostwald equation). For Hanford tank wastes we limit the model fit to pseudoplastic or Newtonian materials (exponent less than or equal to one). When the exponent in the power law model is equal to one, the fluid is a Newtonian fluid and consistency coefficient is the Newtonian viscosity. A fluid with power law behavior does not have a yield stress.

Equation (4.8) is the Herschel-Bulkley model or yield power law curve fit. This model has the greatest number of parameters in the curve, but it is often more detailed than is needed to fit the data. In this model, a yield stress (non-zero intercept with the ordinate) is followed by pseudoplastic behavior (exponent is less than 1). If the yield stress is zero, this model becomes the power law model. If the exponent is one, this model becomes the Bingham plastic model.

## 5.2.2 Shear Strength

Shear strength was measured on core samples taken from the tanks using a shear vane of known dimension as the rotating part of the rheometer. Shear strength is a semi-quantitative measure of the force required to move the sample and is dependent on sample history. Shear strength can be measured directly by slowly rotating a vane immersed in the sample material and recording the resulting torque as a function of time. The measured torque is converted to a shear stress by Eq. 5.1 and 5.2.

$$\tau = T / K \quad (5.1)$$

where

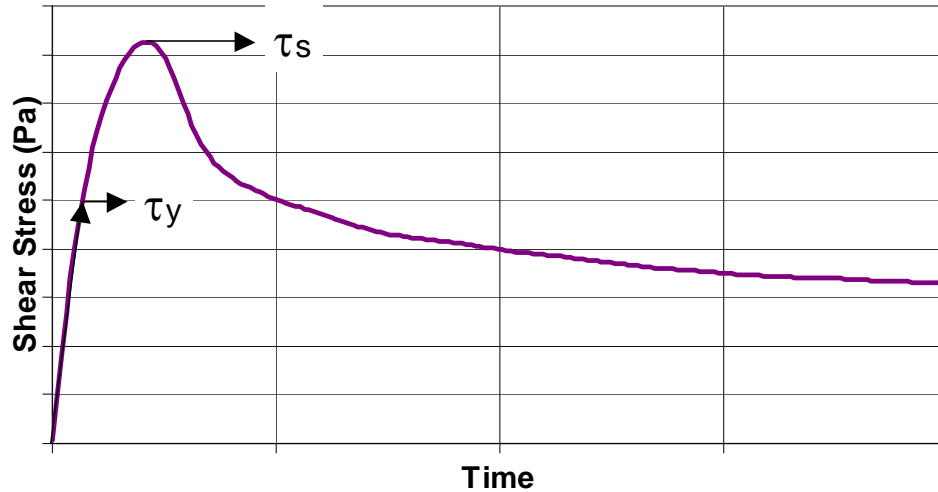
$$K = \frac{\pi D^3}{2} \left( \frac{H}{D} + \frac{1}{3} \right) \quad (5.2)$$

where

- $\tau$  = the calculated shear stress in Pascals
- T = the measured torque in Newton-meters

- K = the shear vane constant in cubic meters
- D = the shear vane diameter in meters
- H = the shear vane height in meters.

A typical stress/time profile is shown in Figure 5.3. The profile shows an initial linear region ( $\tau_y$ ) followed by a nonlinear region, a stress maximum ( $\tau_s$ ), and a stress decay region. The stress maximum is the transition between the visco-elastic and fully viscous flow. Shear strength is defined as the transition between these two flows and is measured at the stress maximum.



**Figure 5.3.** Typical Stress-Versus-Time Profile for a Shear Vane at Constant Shear Rate

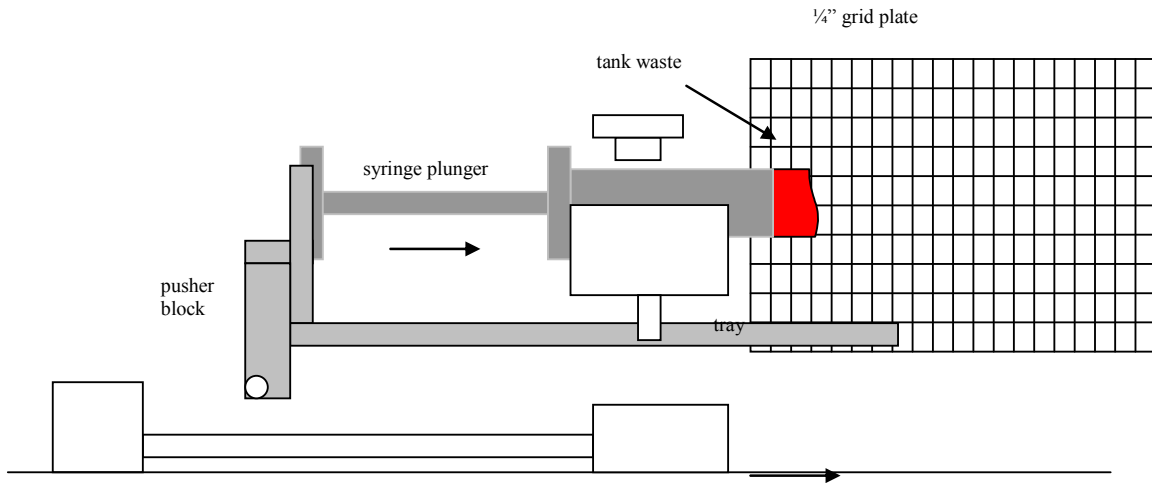
Shear strength was measured on core samples, tank composites, and dilutions that had measurable shear strengths. The diameter and height of the shear vane are typically 1.6 and 3.2 cm, respectively, but other sizes have been used. Details of the vanes are available in the characterization reports. The rotation speed of the shear vane was constant (generally at 0.3 rpm).

To minimize history effects, the shear strength samples were often placed in the sample cup a minimum of 48 hours before the measurement. Sometimes the shear strength measurement was repeated one hour after the initial measurement to provide information about the effect of previous shear on the shear strength of these materials.

### 5.3 Shear Strength Calculation from Extrusion Data

Gauglitz and Aikin (1997) developed a methodology to estimate the shear strength of tank waste materials based on visual observations of horizontal extrusion behavior. A related core extrusion shear strength estimation technique was developed by Rassat et al. (2003). This technique is based strictly on extrusion length and was developed from the simulant extrusion results presented by Gauglitz and Aikin (1997).

An extrusion system has also been developed to make these observations on smaller quantities of waste. In these measurements an infusion syringe pump was modified to mimic the extrusions performed on the core samples from the Hanford tanks (Figure 5.4).



**Figure 5.4.** Mini-Extrusion Design

The pump was controlled by a microstepping motor drive. The motor drive pushed the pusher block against the syringe plunger, displacing the sample. The syringe pump was modified by the addition of a tray mounted directly to the pusher block. As the core was being extruded, the tray moved at the same speed the core was being pushed out.

For the extrusions, 10-mL Becton Dickinson syringes were used. The tips of the syringes were cut off so that the extrusion core would be the inner diameter of the syringe barrel. The cores were approximately 7 cm in length and 1.45 cm in diameter. The height from the bottom of the core to the tray was approximately 1.5 cm. The rate at which the core was extruded was 0.5 in./min. The syringe was filled with the sample in 0.5-mL increments. A microspatula was used to fill the syringe and remove voids in the sample. The syringes were filled a minimum of 72 hours prior to the extrusion. Parafilm was used to minimize drying of the sample. The samples were also placed in a closed plastic bag.

During the extrusions, video images were recorded and then analyzed to estimate the shear strength. To estimate the lengths of the extruded cores, a 6×3-inch grid plate was fabricated and attached to the syringe pump. The camera was placed directly in front of the syringe at a location to capture the entire extrusion. During the extrusions, the camera was not moved.

## 6.0 Physical Properties

Often, physical properties were measured on the same samples used to make rheological measurements. These properties are crucial in correlating the rheological properties of the suspensions in the WTP mixing systems. The physical properties of particular importance in this study include density of the suspension, centrifuged supernatant, centrifuged and settled solids; total solids content in the suspension as well as in the centrifuged and settled solids (both volume and wt% solids); dissolved and undissolved components of the total solids; and zeta potential. Very few data are available on zeta potential of Hanford tank wastes because of the high salt content in the supernatants, which make this measurement difficult on the standard zeta potential instruments available during characterization of these samples. Some of the other physical properties were not measured routinely on all samples; therefore, physical properties for many samples are incomplete.

### 6.1 Density

Density of the bulk sample, supernatant, centrifuged solids, and settled solids generally was calculated from volume and mass measurements. Details of these measurements are provided in the individual reports referenced for each sample. Generally, aliquots of the samples were placed in graduated centrifuge cones or in graduated cylinders and the sample was weighed. After allowing the samples to settle, the volume of the supernatant and solids was determined using the graduations on the centrifuge cones or graduated cylinders. When settled solids density was measured, the supernatant was decanted and placed in a graduated cylinder and weighed to determine the mass of the supernatant. The volume of the supernatant was also measured in the graduated cylinder. The settled solids were also weighed after decanting the supernatant. Settled solids and supernatant density were calculated by dividing the mass by the volume. Settled solids density was sometimes calculated without weighing the settled solids according to Eq. (6.1). In this calculation the density of the centrifuged supernatant was often used as the density of supernatant density used in Eq. (6.1).

$$\rho_{\text{settled solids}} = \frac{m_{\text{sample}} - (\rho_{\text{sup}} \times V_{\text{sup}})}{V_{\text{settled solids}}} \quad (6.1)$$

where

- $\rho_{\text{settled solids}}$  = the density of the settled solids
- $m_{\text{sample}}$  = the mass of the sample used in the measurement
- $\rho_{\text{sup}}$  = the density of the settled supernatant
- $V_{\text{sup}}$  = the volume of settled supernatant
- $V_{\text{settled solids}}$  = the volume of settled solids.

The supernatant was returned to the centrifuge cone, or a new aliquot of the sample was placed in a graduated centrifuge cone, and the sample was centrifuged to separate the liquid (supernatant) in the suspension from the solids. The sediment volume was measured on each sample at the completion of the centrifugation. The supernatant was decanted from the centrifuge cones and transferred to a graduated cylinder. The volume and mass of the decanted supernatant were measured to determine the supernatant



density. The mass of the sediment remaining in the centrifuge cone was also measured. The densities of the supernatant, centrifuged solids, and bulk sample were often calculated from centrifugation data.

In situ liquid density data were obtained by the falling ball rheometer. A reference measurement of the ball in air is subtracted from the density measurements to adjust for the baseline forces associated with measurement. Both ball volume and buoyancy forces are used to calculate the density of waste, as shown in Eq. (6.2). This method is not applicable for materials with yield strengths because the strength of the material supports the ball resulting in an inaccurate buoyancy term (Stewart et al. 1996).

$$\rho = \frac{B_b}{V_b \times g} \quad (6.2)$$

where

$\rho$  = the density of the liquid

$B_b$  = the buoyancy force on the ball

$V_b$  = the volume of the ball

$g$  = the gravitational constant.

## 6.2 Solids Content

Weight percent total solids in the core samples was determined by either thermogravimetric analysis or simple gravimetric analysis methods. Both methods measure the change in the mass as the sample is heated. The mass loss is equated to the mass of water in the sample; therefore, the solids content is equal to the mass remaining in the sample after heating divided by the initial mass of the sample. Solids content is often reported as a percentage of the mass change instead of the fraction of the mass change. Solids content can also be reported in volume percent (volume of the dried solids divided by the volume of the initial sample reported as a percentage). Volume percent solids is often converted from the mass percent solids using the measured densities of the solids and supernatant.

In thermogravimetric analysis, approximately 25 mg of each sample was placed in a platinum, aluminum, or stainless steel pan, and the temperature of the sample was increased from ambient to approximately 550°C at a constant rate (generally 5°C/minute). The mass of the sample (by thermogravimetric analysis) and the change in the temperature of the sample (by differential thermal analysis) in relation to a reference sample (an empty pan of the same metal) were monitored as a function of temperature. These analyses were performed in a flowing air or helium atmosphere. The calibration of the thermal analysis system was checked with a lead or indium standard and calibrated weights. The thermogravimetric approach is typically used to distinguish free water from waters of hydration and, possibly, decomposition of solids at the higher temperatures.

A simpler gravimetric weight percent solids measurement is made by drying samples of known mass in a drying oven at 105°C. Greater than 2 g of material were weighed and then dried to obtain the total solids concentration. The mass of the sample before and after drying was measured.

Dissolved solids and undissolved solids content was calculated from the solids content measured in the supernatant (dissolved solids), total solids content (solids content of the bulk sample), and the fraction

of supernatant in the sample measured after centrifugation or filtration. The equations used for calculating weight percent dissolved solids and undissolved solids are shown in Eq. (6.3) and (6.4), respectively. Weight percent undissolved solids is converted to volume percent using the densities of the undissolved solids and bulk sample.

$$DS \text{ (wt\%)} = \left( \frac{\text{Supernatant mass}}{\text{Sample mass}} \right) \times \text{Supernatant Solids Content} \quad (6.3)$$

$$UDS \text{ (wt\%)} = TS \text{ (wt\%)} - DS \text{ (wt\%)} \quad (6.4)$$

where

- DS = the percent dissolved solids
- UDS = the percent undissolved solids
- TS = the percent total solids.

### 6.3 Zeta Potential

Zeta potential is the electrostatic potential at the surface of shear and is calculated from the electrophoretic mobility (velocity per unit of electric field strength). The surface of shear is not the surface of the particle, but extends from the particle out into solution to include the solution that moves with the particle (hydrodynamic size). A positive mobility (zeta-potential) means the surface of the particle is positively charged, a negative mobility means the surface is negatively charged, and a mobility value of zero means that the velocity is zero, which implies that electrostatic repulsion is small.

A charged solid-liquid interface (electrical double layer) is created between the charged particle and the liquid. In this electrical double layer, the concentration of the counter ions (ions in solution with the opposite charge as the particle surface) is higher near the particle and decrease steadily to the concentration in the bulk liquid. The thickness of this double layer is dependent upon the temperature, the dielectric constant of the liquid, and the ionic strength of the bulk liquid. For 1:1 electrolytes such as KCl at a bulk concentration of 1 mM, the double-layer thickness is approximately 10 nm. As the concentration of the electrolyte increases, the double layer thickness and the range of the repulsive forces between the molecules decreases.

Zeta potential is calculated from electrophoretic mobility using a theoretical model. Two classic models (Hückel and Smoluchowski equations) are used for these calculations. The Hückel equation is used for simple ions where the hydrodynamic radius is very small, and the Smoluchowski equation is used for very large particles. For most colloidal particles of interest dispersed in water, it is not easy to satisfy either model; therefore, mobility is related to zeta potential by a model-dependent function. Generally, these functions are more accurate for 1:1 electrolytes at  $10^{-3}$  to  $10^{-2}$  M salt.

The zeta potential of tank waste was measured by the Brookhaven Instrument Corporation's ZetaPlus zeta potential analyzer. In this system, a laser beam passes through the dilute sample between two electrodes that create an electric field. The particles in solution scatter the laser light as they move in this electric field.

The light that is scattered by the particles is Doppler-shifted because the scattering particles are moving in the electric field due to the charge on their surface. The Doppler shift is proportional to the velocity (both rate and direction) of the particles in this electric field, which is proportional to the electrophoretic mobility of the particles (Eq. 6.5).

$$\mathbf{V}_s = \mu_e \mathbf{E} \quad (6.5)$$

where

$\mathbf{V}_s$  = the average velocity of the TiO<sub>2</sub> particles

$\mu_e$  = the electrophoretic mobility

$\mathbf{E}$  = the electric field.

Because the ionic strength in most tank waste samples is extremely high (salt contents > 1 M), zeta potential was difficult to measure in the standard instruments available when most samples were characterized.

## 7.0 Sedimentation Measurements

Settling behavior of tank waste samples including dilutions of tank waste samples was determined by both gravity settling and centrifugation. Aliquots of the samples were allowed to settle in graduated cylinders or graduated centrifuge cones. The sediment volume and total volume of the sample aliquots were recorded as a function of time. In a few reports the height of the sediment bed and total sample were also recorded as a function of time. The samples were then centrifuged and the volume of the centrifuged supernatant and centrifuged solids were recorded. Details of the time and force used in centrifugation are reported in the individual characterization reports. The mass and volume of clear supernatant, centrifuged and settled solids, and total sample were generally determined for each aliquot at the completion of settling and centrifugation.

As the samples settled, an interface developed between the turbid suspension and clear supernatant. The sediment volume is the volume from the bottom of the suspension column to the interface between the clear supernatant and the cloudy suspension. Under the force of gravity, the solids in the suspension sank to the bottom of the cylinder, forming a sludge layer and a clear supernatant layer. The final sediment bed volume was measured after no significant change was observed in the height of this sludge layer over the prescribed time described in the individual characterization reports. The volume percent settled solids were then determined by dividing the final sediment bed volume by the total volume of the slurry.

The settling rate measured by this method is controlled by the settling rate of the smallest particles in the suspension. In a suspension with particles of uniform size, all of the particles will settle at the same rate, and a sharp boundary will exist between the clarified portion of the settling system and the fraction of the system where the particles are still settling. Hanford tank wastes are polydisperse systems, where each size fraction or material type (different particle densities) settles at its own characteristic velocity. The boundary between the clarified supernatant and the settling fraction of the system may be a diffuse region. The rate at which a particle settles in a suspending liquid depends on the size, shape, solvation, and density of the particle as well as the density and viscosity of the suspending medium. Stokes law provides a mathematical expression of the terminal settling velocity for spherical particles (Eq. 7.1). Asymmetry in the particle shape and solvation of the particle increase the friction factor of the settling particle, decreasing the settling rate of a particle of given mass compared to a spherical, unsolvated particle.

$$v = \frac{2r^2(\rho_p - \rho)g}{9\eta} \quad (7.1)$$

where

- $v$  = the terminal velocity of the particle
- $r$  = the radius of the particle
- $\rho_p$  = the density of the particle
- $\rho$  = the density of the suspending medium
- $g$  = the gravitation force
- $\eta$  = the viscosity of the suspending medium.

Interstitial liquid associated with the settled solids was further separated from the solids by centrifugation. The sediment volume was measured on each aliquot as function of time at a given force. Data for many samples were only recorded at a single duration. The volume percent centrifuged solids was then determined by dividing the sediment volume by the total volume of the slurry. The supernatant was decanted from the centrifuge cones, and the decanted supernatant and sediment were weighed. The weight percent supernatant and centrifuged solids were calculated by dividing their mass by the mass of the aliquot.

## 8.0 Rheology and Physical Properties Data

Appendix A is a compilation of the available rheology data for Hanford tank wastes. These data include in situ as well as laboratory analysis of samples removed from the tanks. If rheology data were available for samples, the physical properties of these samples were included with the rheology data. Settling rate as a function of time was included when available. Composition of the solids phases as determined by ESP was also included for each rheology sample.

The tables in Appendix A are organized by tank with a column for each sample for which rheology was obtained. There is a brief description of each sample along with a reference for the source of the rheology data. The model or basis used for interpreting the solid composition data is based on the ionic strength of the supernatant. The choices for this basis included salty, salt free, washed, leached, liquid, and supernatant. No distinction is made between salt-free and washed or liquid and supernatant.

### 8.1 Model Basis

Salty is used to describe samples that were untreated; therefore, it is assumed that the supernatant and solids composition is not changed from what is observed in tank. Rheology measurements on many samples were performed at multiple temperatures, and measurements made near tank temperature will be closest to this approximation. As temperatures decrease, dissolved solids may precipitate, and the solid content may increase. At elevated temperatures, solids may dissolve in the suspending medium, and the concentration of undissolved solids may decrease.

Salt free and washed models describe samples that were washed or diluted with water or supernatant. Washing or water dilutions decrease the salts in solution and may result in decreased undissolved solids contents. Total solids content will also decrease upon washing or diluting the sample. Washing the waste may also selectively remove specific solids from the settled solids. Because of changes in the composition of the solids and supernatant, washing and diluting tank wastes may significantly affect the rheological properties of the samples.

Leached model describes those tank samples that were washed in dilute NaOH/NaNO<sub>2</sub>, followed by washing in concentrated NaOH to remove Cr, Al, and P from the sample, and then washing with dilute NaOH/NaNO<sub>2</sub> to remove any leached Cr, Al, or P remaining in the sample. The removal of Al and P from the sample may significantly affect the rheology of the suspension.

Liquid and supernatant models were used to describe the supernatant obtained from centrifugation or settling of slurries. They also describe core and dip samples that consisted of liquid or supernatant. These samples provide additional information on the rheological properties of the suspending medium.

## 8.2 Solid Phases

The average compositions of the solid and liquid phase in each tank were included in the tables in Appendix A. These compositions were derived from modeling carried out using the ESP<sup>(a)</sup> chemical thermodynamic model as described in WTP-RPT-153 (Wells et al 2007). The ESP predictions constitute the only phase composition information that 1) is available for all 177 tanks and 2) was prepared using a consistent method for all 177 tanks. It was therefore appropriate and advantageous to draw on this database in devising a sludge phase composition for transfer system design. However, this application of ESP had certain characteristics that should be noted:

- Compositions were calculated on a whole-tank basis, as if all the different layers of waste had been mixed and allowed to come to equilibrium.
- ESP is an equilibrium model and is not expected to predict the correct concentration of any compounds that have not yet come to equilibrium with an in-tank chemical environment different from those in which they formed (e.g., different temperature, pH, etc.).
- In the 2002 study, certain compounds were excluded from precipitating to reflect kinetic limitations or sometimes to reduce computational time or avoid nonconvergence of the solution algorithm. A significant example is boehmite, which was excluded because, had it been included, it would have been thermodynamically preferred to gibbsite in all wastes. Because gibbsite is actually dominant due to kinetic constraints that prevent boehmite from forming at lower temperatures, the databank excluded boehmite from forming at a temperature less than 100°C.
- Because of computational time constraints, Redox equilibrium was not calculated on a tank-by-tank basis in the 2002 study; rather, expert judgment and generic-composition runs of ESP were used to fix the metal oxidation states in all tanks. Iron was fixed as Fe<sup>+3</sup>, manganese as Mn<sup>+2</sup>, chromium as Cr<sup>+3</sup> or Cr<sup>+6</sup>, and so forth. Thus, the ESP predictions could not include compounds formed by metals in any other oxidation states.
- The study assigned compounds to the “trace analytes” (including thorium, cadmium, copper, tin, and many others) without employing the ESP model; thus, these metals are not present in the compounds in the ESP-predictions database.
- Thermodynamic data were not available for all the compounds that could potentially form in the tank waste, which led to the omission of some compounds.

The solids predicted by the ESP chemical thermodynamic model for the tank-average solid phase were taken as a best approximation, although [as noted in Wells et al. (2007)] there were cases in which the ESP model predicted solids that were not observed, and others in which observed solids were not predicted. Only one compound modification was made to the ESP output: all aluminum hydroxide predicted by ESP in tanks containing Redox boiling waste was substituted with boehmite on an equivalent-Al basis, as in Wells et al. (2007). Aluminum hydroxide/oxide predicted in other tanks was considered to be gibbsite.

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(a) ESP was supplied and developed by OLI Systems, Inc., Morris Plains, New Jersey.

The ESP model, as used, predicted the concentration of each solid in the waste on a normalized basis. In other words, the model predicted the relative masses of different solids, and the relative volumes and masses of total liquid and total solid, but not the absolute masses or volumes in a tank. The absolute mass of each solid–phase compound in a tank was calculated for the present study by combining the modified ESP results with BBI volumes, using Eq. (8.1):

$$M_S = c_S V \phi_{ESP} \quad (8.1)$$

where

- $c_S$  = mass of compound per volume of solid phase
- $V_S$  = solid phase volume in the tank
- $\phi_{ESP}$  = ESP-predicted fraction of solid phase, average of all the waste in the tank
- $V$  = total waste volume in the tank as defined by the 2002 BBI.

The solid volume calculated by the above equation contains some uncertainty because of uncertainty in the parameters and because potential retained gas volume is not accounted for. The portion of the volume  $V$  that is not solid phase is liquid volume, which includes both the interstitial liquid in the bulk solids layers and any supernatant that may be present. The volume of each compound in the solid phase was calculated by dividing the mass of each compound by the density. All the densities discussed were taken from the *Handbook of Chemistry and Physics* (CRC 1975), as in Wells et al. (2007), except where otherwise noted.

The ESP-predicted solid-phase compositions were on a “salty” basis; that is, the water-soluble sodium salt solids were included. These compositions were used to calculate a second composition that was on a “salt-free” basis, where only the insoluble metal compounds were retained in the solid phase.

Physical property measurements from tank characterization reports were used to provide the mass fraction of undissolved solids for a particular slurry sample. This was multiplied by the ESP solid phase speciation to produce the mass fraction of an ESP species in the slurry sample. Slurry densities from physical property measurements along with literature values for crystal density of the ESP phases were then used to convert the mass fraction to volume percent undissolved solids in the slurry sample.

### 8.3 Rheological Data

Rheological data included the temperature, instrument, source of the data, and all applicable model fits for the rheological data. Details about the rheological measurements can be obtained from the individual references. Correlation coefficients for each curve fit are also included with each model used for the available data. A description of the curve fits is provided in Section 4, Rheology Theory.

### 8.4 Physical Property Data

Physical property data may be obtained from a separate reference than was used to report the rheology data, but physical properties data do represent the properties of the sample used to perform the rheology. The physical properties reported included bulk, supernatant, centrifuged solids, settled solids,



and particle (listed as solids) densities; volume and weight percent settled solids (also listed as settled supernatant which is just 100% minus the percent settled solids) and centrifuged solids; and solids content of the supernatant (dissolved solids), centrifuged sludge, and bulk sample (total solids); and the percent undissolved solids. Zeta potential is also listed in the table, but only minimal data were obtained on zeta potential of tank waste samples. A detailed description of these measurements is provided in Section 6. If available, the temperature at which these physical properties were measured was also reported. Details of these data are provided in the reference associated with each sample.

## **8.5 Settling Data**

Gravity settling data is reported as the volume of the sediment bed as a function of time (up to 72 hours) for each sample. The total volume of the aliquot in the settling column (initial volume) is also recorded for each sample. Settling data is also reported for multiple temperatures if it is available. A more detailed description of the method used for gravity settling is described in Section 7.

## **8.6 Particle Size Data**

Particle size data used in this report are obtained from a report prepared earlier this year, *Estimate of Hanford Waste Insoluble Solid Particle Size and Density Distribution* (Wells et al. 2007). No modifications were made to the data reported in that document. The data reported in the tables are the particle diameter for cumulative volume percents ranging from 1 to 99%.

## **8.7 Shear Strength Data**

Shear strength data are reported as a function of gelation time. Only limited data were obtained at discrete gelation times. Most of the shear strength data were obtained for samples that had remained undisturbed for a minimum of three days. Inserting the shear vane did not constitute disturbing the sample for this report. A more detailed description of the methods used to obtain shear strength is provided in Section 5. The data reported include measurements from the ball rheometer and laboratory measurements using a vane geometry. Calculation of shear strength from core extrusions is not included in this report.

## 9.0 Viscosity Model

Hanford liquid supernatant can be characterized rheologically as a Newtonian fluid. While the chemical composition of the aqueous waste has a significant effect on the viscosity of the supernatant liquid, the model described in this section attempts to model the Hanford supernatant viscosity as a function of only liquid density and temperature. Liquid density was selected as an independent variable in this model because it is relatively easy to measure and directly scales with dissolved species concentration.

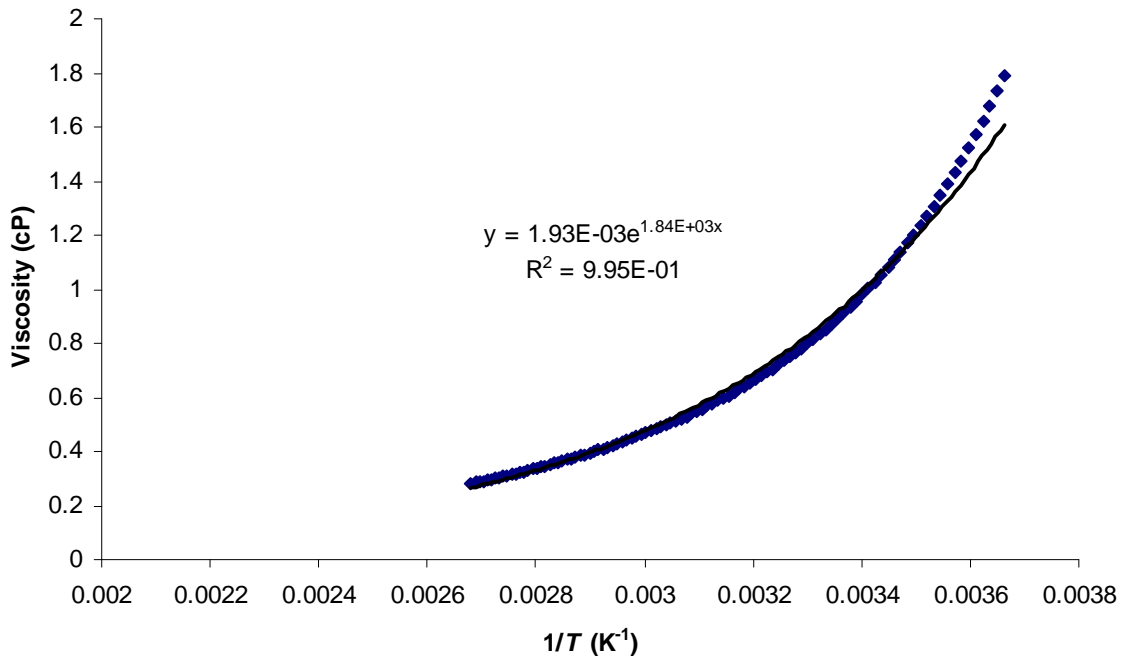
Temperature is known to have a large effect on liquid viscosity. The Andrade correlation is a mathematical relationship often used when evaluating the relationship between increasing temperature and decreasing viscosity of liquids. It is not accurate for high-temperature fluids or highly polar mixtures. This equation is shown as Eq. (9.1):

$$\eta = Ae^{\frac{B}{T}} \quad (9.1)$$

where

- $\eta$  = the Newtonian viscosity in cP
- $T$  = temperature in Kelvin (K)
- $A$  (in cP) and  $B$  (in K) = fitting parameters associated with molecular structure.

A plot of the viscosity of water as a function of temperature is shown in Figure 9.1. For water the Andrade equation parameters are 0.0019 cP and 1800K for  $A$  and  $B$ , respectively.



**Figure 9.1.** Viscosity of Water at Various Temperatures

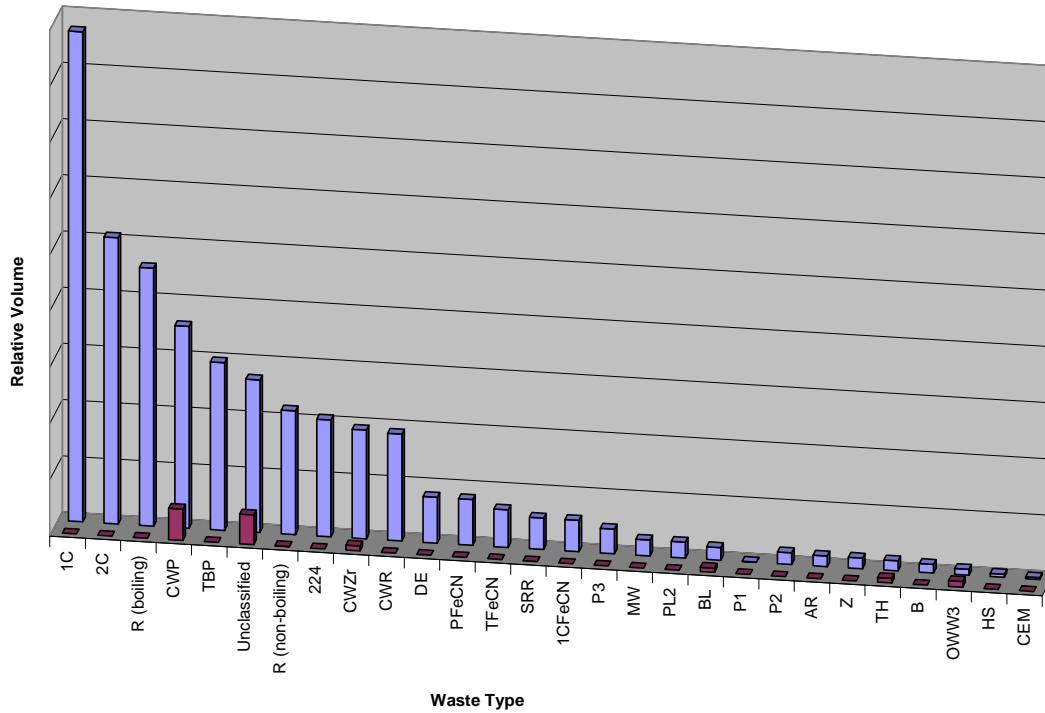
Liquid viscosity data from 8 different Hanford tanks was analyzed as a function of liquid density, temperature, and dilution with water (salt content). The tanks for which this data was available are listed in Table 9.1. Relative volumes of the waste types comprised by these tanks are shown in Figure 9.2. Several sludge waste types are not represented in this analysis due to a lack of appropriate data.

**Table 9.1.** Liquid Viscosity Data for Hanford Tank Wastes

Tank	Density (g/mL)	Dilution	Temperature (°C)	Viscosity (cP)	
241-AN-103	1.42	Supernatant from 80% Dilution of Settled Solids	29	11.6	
	1.42		45	6.7	
	1.42		65	4.6	
	241-AN-103	1.46	26% Dilution of Supernatant	29	7.8
		1.46		45	5.4
		1.46		65	3.7
	241-AN-103	1.52	10% Dilution of Supernatant	29	8.8
		1.52		45	5.9
		1.52		65	4
		1.58	Undiluted Supernatant	29	27.4
1.58		45		13	
1.58	65	7.6			
241-AN-104	1.26	Undiluted Permeate	25	3.5	
	1.31	Supernatant from 80% Dilution of Settled Solids	25	17.5	
	1.31		45	8.1	
	1.31		65	5.4	
	1.42	Undiluted Supernatant	25	16.9	
	1.42		45	8.1	
1.42	65		4.6		
241-AN-105	1.35	20% Dilution of Supernatant	25	9.4	
	1.35		45	4.2	
	1.35		65	2.4	
	1.42	Undiluted Supernatant	25	12.3	
	1.42		45	6.3	
1.42	65	3.5			
241-AP-104	1.26	Undiluted Supernatant	25	3.7	
	1.26		40	2.4	
241-AW-101	1.38	Supernatant from 50% Dilution of Tank Composite	25	11.5	
	1.38		45	5.4	
	1.38		65	3.6	
	1.42	Supernatant from 80% Dilution of Settled Solids	25	6.0	
	1.42		45	3.0	
	1.42		65	1.8	
	1.52	Undiluted Supernatant	25	22.0	
	1.52		45	8.0	
1.52	65	5.4			
241-AY-102	1.13	Centrifuged Liquid Composite	27	1.8	
	1.13		45	1.1	
	1.13		65	0.3	
241-C-104	1.24	Undiluted Supernatant	25	1.3	
	1.24		45	1.3	
	1.24		65	1.4	
241-S-112	1.16	20% Dilution of 2nd Dissolution Contact <sup>(a)</sup>	20	2.0	
	1.16		35	1.8	
	1.16		50	1.4	
	1.36	20% Dilution of 1st Dissolution Contact <sup>(b)</sup>	20	5.7	
	1.36		35	4.0	
	1.36		50	2.9	

(a) The second contact was accomplished by mixing 30 g of residue from the first contact in 70.5 g of water at 50°C.

(b) The first contact was accomplished by mixing 82 g of waste with 50 g of water at 50°C.



**Figure 9.2.** Relative Waste Volumes Used in the Analysis of Liquid Viscosity as a Function of Sludge Waste Types

Figure 9.3 is a plot of the Hanford liquid viscosity as a function of density. During the multidecade Hanford tank waste characterization effort, measurements were not performed at consistent temperatures. Therefore, data are grouped in 15°C temperature increments starting at 20° to 35°C and ending at 80° to 95°C. In addition, the data are grouped according to whether the sample was from a tank waste composite [as-received (AR)] or diluted with water (Dil). Exponential fits to these data for each temperature group were also obtained and are shown in a log plot of viscosity as a function of liquid density minus one (second plot in Figure 9.3). These data indicate that liquid density should be maintained below 1.4 to 1.5 g/mL to avoid exceeding the 15 cP liquid viscosity bound found in Poloski et al. (2003a). The coefficients for these exponential fits were constrained to produce the viscosity of water according to the Andrade correlation when sample density is unity.

At constant density, the parameters of the exponential fits vary with temperature. Assuming that the model takes the form of the Andrade correlation at each liquid density, the viscosity of the supernatant in the Hanford tanks can be correlated to density according to:

$$\eta = \left(m_1 e^{b_1(\rho-1)}\right) e^{(m_2(\rho-1)+b_2)/T} \quad (9.2)$$

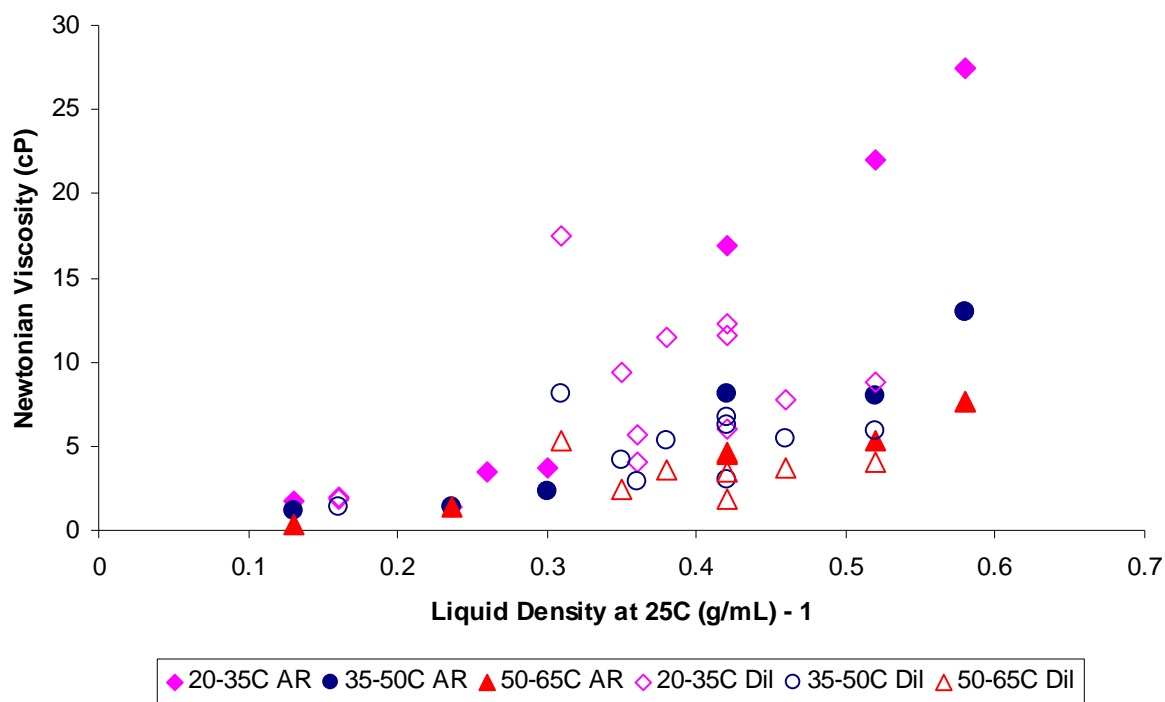
where

$\eta$  = the Newtonian viscosity in cP

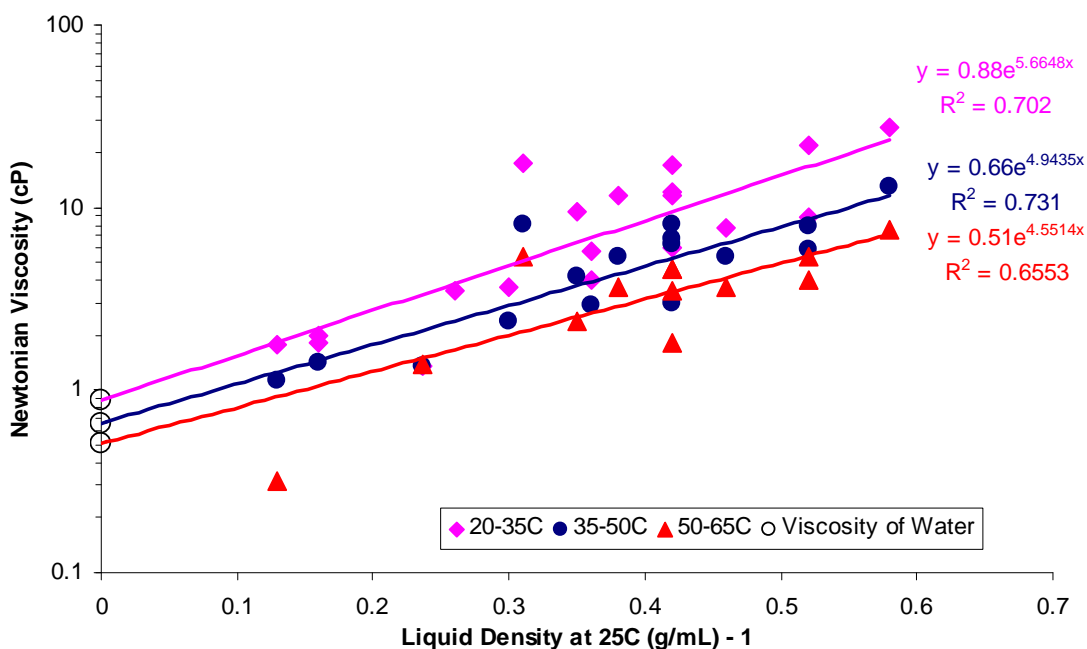
$T$  = temperature in Kelvin

$\rho$  = the liquid density in g/mL

$m_1$  = 0.00216 cP



(a) Data grouped according to dilution and temperature.



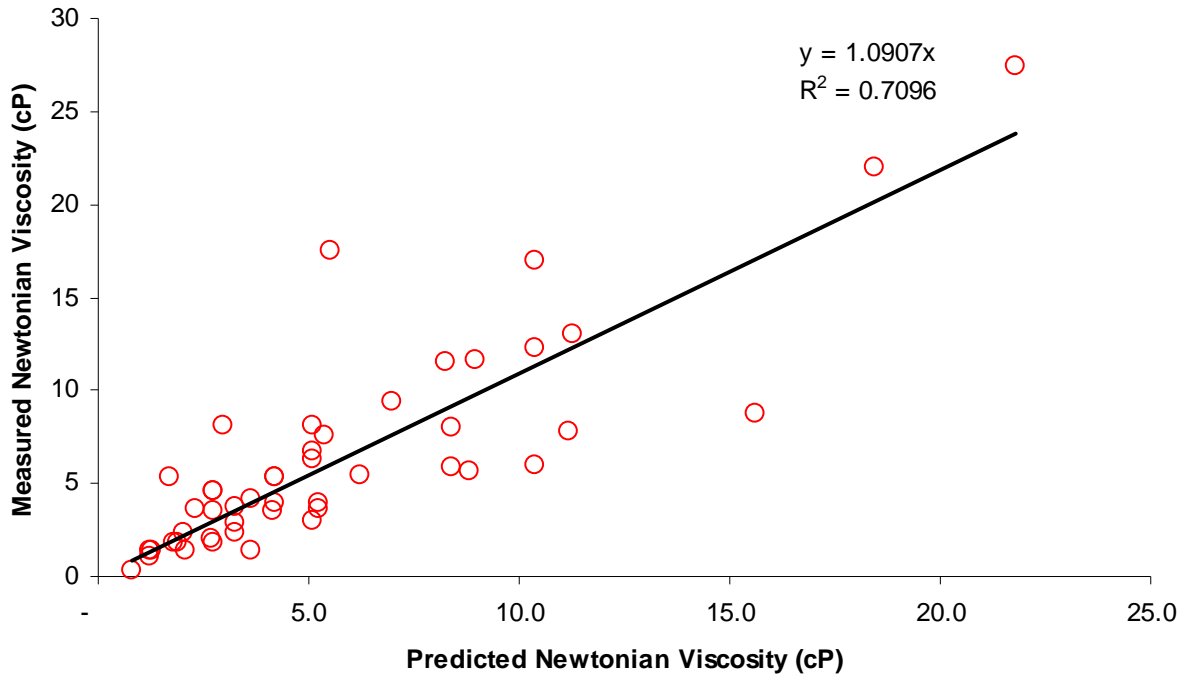
(b) Exponential fits at various temperatures

**Figure 9.3.** Viscosity of Hanford Supernatant at Various Densities and Temperatures

$$b_1 = -6.69 \text{ (g/mL)}^{-1}$$
$$m_2 = 3700\text{K}\cdot\text{(g/mL)}^{-1}$$
$$b_2 = 1810\text{K}.$$

When the liquid density is unity, this equation reduces to the Andrade correlation for water.

Figure 9.4 is a parity plot of the measured and predicted viscosities. Based on this correlation, on average, measured viscosity is biased by 9%.



**Figure 9.4.** Parity Plot of Measured and Predicted Hanford Supernatant Liquid

## 10.0 Sedimentation Model

Hanford tank waste was observed to settle in the “zone” or “hindered” settling regime. This regime occurs when interacting particles settle as a mass and is common in the wastewater industry. Hindered settling is characterized by the settled-solids layer height decreasing from the fully suspended volume to a final settled-solids volume. Several models have been developed to predict the performance of sludge in a settling system based on laboratory-scale sedimentation column data. One of the more recent models is described by Renko (1996, 1998) and is shown in Eq. (10.1).

$$\frac{z}{z_0} = \frac{C\phi_0}{\alpha} + \left(1 - \frac{C\phi_0}{\alpha}\right) e^{\frac{-\alpha}{\phi_0 z_0} t} \quad (10.1)$$

where

- $z$  = the interface height (m) at time  $t$  in hours
- $z_0$  = the initial interface height (m)
- $\phi_0$  = the initial solids concentration of the suspended sample (volume fraction)
- $\alpha$  and  $C$  = fitting parameters in  $\text{m/hr}^{-1}$ .

When sedimentation begins, the interface height ( $z$ ) is equal to the initial interface height ( $z_0$ ). As time goes to infinity, the interface height approaches  $\frac{C\phi_0 z_0}{\alpha}$ . Because the average solids concentration varies with interface height, as shown in Eq. (10.2), the maximum solids concentration ( $\phi_{\text{max}}$ ) achieved through sedimentation is  $\frac{\alpha}{C}$ .

$$\phi = \frac{\phi_0 z_0}{z} \quad (10.2)$$

Based on these relationships, Eq. (10.1) can be rewritten in terms of average solids concentration as shown in Eq. (10.3).

$$\phi = \left[ \frac{C}{\alpha} + \left( \frac{1}{\phi_0} - \frac{C}{\alpha} \right) e^{\frac{-\alpha}{\phi_0 z_0} t} \right]^{-1} \quad (10.3)$$

The data collected in this report contains 58 sedimentation curves over 17 waste tanks and eight waste types. Each sedimentation curve was fit to Eq. (10.1), and the fitting parameters  $\alpha$  and  $C$  are reported in Table 10.1. Values for the initial solids concentration ( $\phi_0$ ) were estimated from physical property data. Values for the initial sediment height ( $z_0$ ) were unknown for many of the data because they only reported volume (or vol%) rather than height. However, most measurements were performed in small graduated cylinders or graduated centrifuge cones with a total volume of 20–50 mL; therefore, an initial height of 10 cm was assumed in all calculations. This is similar to the data where sediment height as well as sediment volume was provided (Morrey and Tingey 1996).

**Table 10.1.** Sedimentation Model Input and Fitting Parameters for Hanford Tank Waste

Tank	Waste Type	$\phi_0$ vol%	$z_0$ mm	$C$ mm/hr	$\alpha$ mm/hr	$\phi_{max}$ vol%
B-202	224	0.8%	100	21.7	0.43	2.0%
B-202	224	0.8%	100	17.0	0.34	2.0%
B-202	224	0.8%	100	36.1	0.68	1.9%
B-202	224	0.9%	100	17.2	0.32	1.9%
B-202	224	0.9%	100	19.8	0.38	1.9%
B-202	224	1.0%	100	25.3	0.64	2.6%
B-202	224	2.0%	100	12.2	0.32	2.6%
B-202	224	2.1%	100	11.8	0.31	2.6%
B-202	224	2.0%	100	13.3	0.31	2.3%
B-202	224	2.0%	100	9.6	0.25	2.6%
B-202	224	2.3%	100	9.4	0.25	2.6%
B-202	224	2.3%	100	9.6	0.28	2.9%
<b><i>B-202 Average values →</i></b>				<b>16.9</b>	<b>0.38</b>	<b>2.3%</b>
B-203	224	0.4%	100	53.4	0.55	1.0%
B-203	224	1.8%	100	6.1	0.13	2.1%
B-203	224	1.8%	100	6.1	0.13	2.1%
<b><i>B-203 Average values →</i></b>				<b>21.8</b>	<b>0.27</b>	<b>1.7%</b>
T-111	224	0.1%	100	9.4	0.01	0.1%
T-111	224	0.2%	100	7.0	0.02	0.3%
T-111	224	1.9%	100	1.9	0.05	2.6%
<b><i>T-111 Average values →</i></b>				<b>6.10</b>	<b>0.027</b>	<b>1.0%</b>
T-203	224	0.4%	100	28.9	0.27	0.9%
T-203	224	1.3%	100	4.7	0.07	1.4%
<b><i>T-203 Average values →</i></b>				<b>16.8</b>	<b>0.17</b>	<b>1.2%</b>
T-204	224	0.4%	100	91.7	0.75	0.8%
T-204	224	1.5%	100	4.4	0.07	1.7%
<b><i>T-204 Average values →</i></b>				<b>48.1</b>	<b>0.41</b>	<b>1.3%</b>
BX-107	1C	0.4%	100	13.4	0.17	1.3%
BX-107	1C	0.5%	100	26.0	0.29	1.1%
BX-107	1C	0.5%	100	20.9	0.27	1.3%
BX-107	1C	2.2%	100	12.4	0.50	4.1%
BX-107	1C	2.6%	100	18.4	0.73	4.0%
BX-107	1C	2.7%	100	13.9	0.56	4.0%
<b><i>BX-107 Average values →</i></b>				<b>17.5</b>	<b>0.42</b>	<b>2.6%</b>
C-110	1C	0.3%	100	9.7	0.08	0.8%
C-110	1C	0.5%	100	9.2	0.13	1.4%
C-110	1C	1.5%	100	7.8	0.17	2.2%
C-110	1C	2.5%	100	11.0	0.46	4.2%
<b><i>C-110 Average values →</i></b>				<b>9.4</b>	<b>0.21</b>	<b>2.2%</b>
T-107	1C	3.4%	100	10.7	1.02	9.6%
T-107	1C	7.5%	100	5.3	0.59	11.1%
<b><i>T-107 Average values →</i></b>				<b>8.0</b>	<b>0.81</b>	<b>10.4%</b>
T-110	2C	0.3%	100	20.1	0.25	1.2%
T-110	2C	1.4%	100	12.7	0.39	3.1%
T-110	2C	3.5%	100	1.1	0.05	4.5%
<b><i>T-110 Average values →</i></b>				<b>11.3</b>	<b>0.23</b>	<b>2.9%</b>



**Table 10.1** (contd)

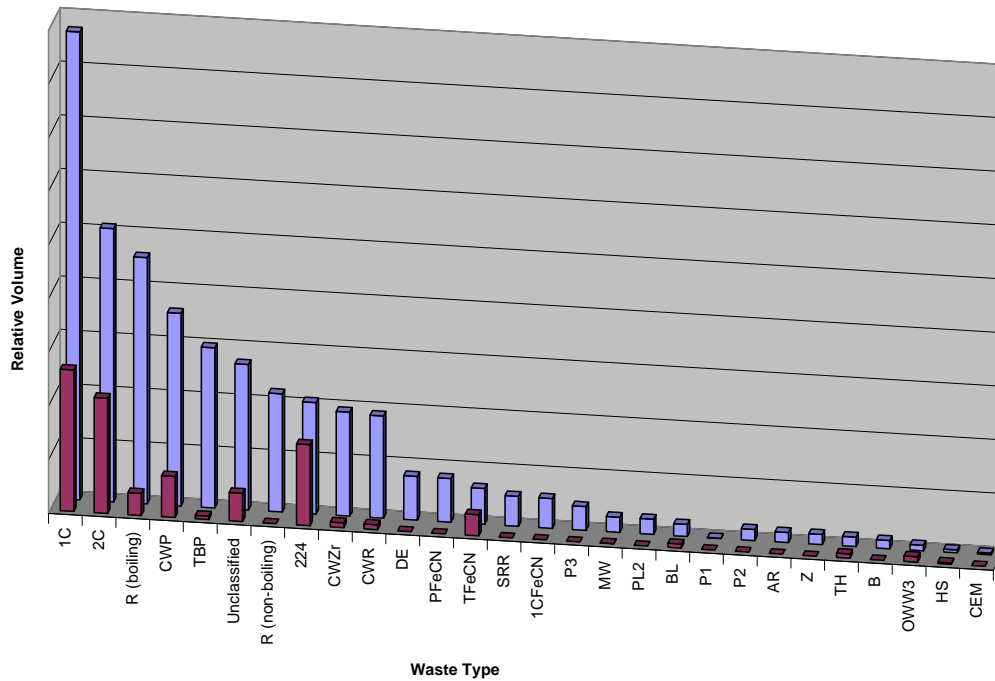
Tank	Waste Type	$\phi_0$ vol%	$z_0$ mm	$C$ mm/hr	$\alpha$ mm/hr	$\phi_{max}$ vol%
AN-104	A2SlrSlr	0.4%	100	6.1	0.14	2.3%
AN-104	A2SlrSlr	0.9%	100	7.4	0.68	9.2%
AN-104	A2SlrSlr	3.2%	100	20.7	1.17	5.6%
AN-104	A2SlrSlr	4.5%	100	19.8	1.05	5.3%
<b>AN-104 Average values →</b>				<b>13.5</b>	<b>0.76</b>	<b>5.6%</b>
AN-105	A2SlrSlr	0.7%	100	8.0	0.48	6.0%
AN-105	A2SlrSlr	4.2%	100	1.8	0.54	30.1%
AN-105	A2SlrSlr	8.2%	100	5.0	0.80	16.0%
AN-105	A2SlrSlr	10.5%	100	3.9	0.99	25.1%
<b>AN-105 Average values →</b>				<b>4.7</b>	<b>0.70</b>	<b>19.3%</b>
C-104	CWP	2.1%	100	4.6	0.44	9.7%
C-104	CWP	3.0%	100	4.3	0.34	7.8%
C-104	CWP	5.1%	100	3.8	0.41	10.7%
<b>C-104 Average values →</b>				<b>4.2</b>	<b>0.40</b>	<b>9.4%</b>
T-102	CWP	2.1%	100	22.5	4.66	20.7%
T-102	CWP	4.7%	100	37.6	10.33	27.5%
<b>T-102 Average values →</b>				<b>30.1</b>	<b>7.5</b>	<b>24.1%</b>
S-104	R (boiling)	2.3%	100	9.0	0.25	2.7%
S-104	R (boiling)	2.8%	100	8.6	0.37	4.3%
S-104	R (boiling)	8.7%	100	5.1	0.50	9.8%
<b>S-104 Average values →</b>				<b>7.6</b>	<b>0.37</b>	<b>5.6%</b>
C-109	TFeCN	2.2%	100	16.1	0.82	5.1%
C-109	TFeCN	3.5%	100	14.3	0.58	4.1%
<b>C-109 Average values →</b>				<b>15.2</b>	<b>0.70</b>	<b>4.6%</b>
C-112	TFeCN	2.2%	100	8.6	0.42	4.9%
C-112	TFeCN	5.9%	100	1.9	0.17	8.8%
<b>C-112 Average values →</b>				<b>5.3</b>	<b>0.30</b>	<b>6.9%</b>
AY-102	Unclassified	7.8%	100	6.0	0.80	13.3%

The data presented in Table 10.1 can be grouped according to waste type. A summary table of the fitting parameters for each waste type is shown in Table 10.2.

**Table 10.2.** Sedimentation Parameters for Each Waste Type

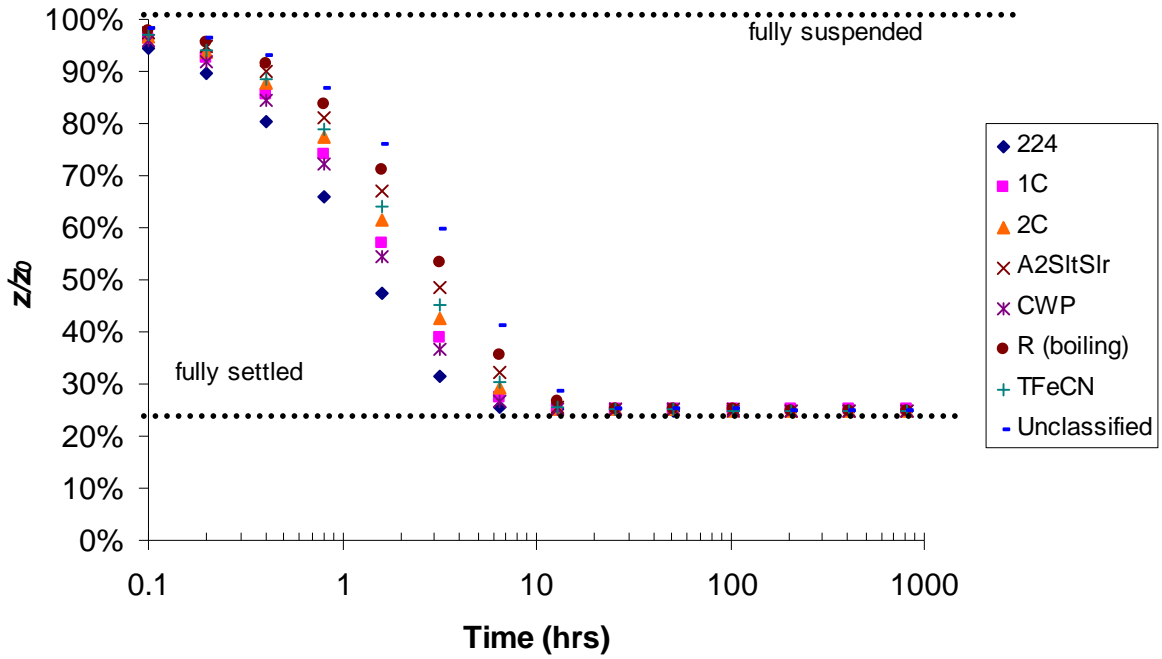
Waste Type	Avg $C$ (mm/hr)	Avg $\alpha$ (mm/hr)
224	18.9 ± 20.2	0.3 ± 0.2
1C	13.2 ± 5.9	0.4 ± 0.3
2C	11.3 ± 9.6	0.2 ± 0.2
A2SlrSlr	9.1 ± 7.2	0.7 ± 0.3
CWP	14.6 ± 15.1	3.2 ± 4.4
R (boiling)	7.6 ± 2.2	0.4 ± 0.1
TFeCN	10.2 ± 6.4	0.5 ± 0.3
Unclassified	6.0 ± not measured	0.8 ± not measured

Several of the waste types are not represented in this modeling activity because appropriate data was not available. The gaps in the waste types modeled are shown in Figure 10.1. The relative volume of each waste type in the 17 waste tanks modeled (red bar in the front of the graph) is compared to the total volume of waste associated with those waste types (blue bar in the back of the graph). The volume of waste in each tank for each waste type was determined using the TWINS database.

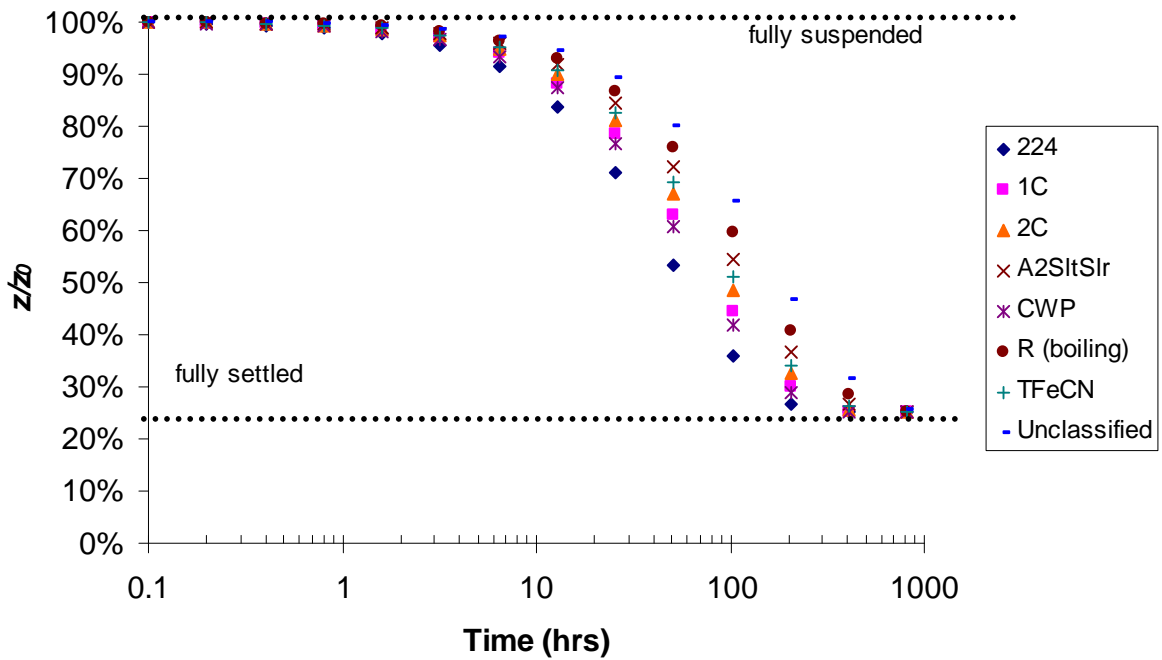


**Figure 10.1.** Gaps in Data Available for Sedimentation Modeling as a Function of Waste Type

From Eq. (10.1) and (10.3), initial interface height,  $z_0$ , and initial solids concentration,  $\phi_0$ , are input parameters to determine the interface level and solids concentration as a function of time. The average values from Table 10.1 were used to calculate interface height as a function of time at an initial solids concentration equivalent to a 3:1 dilution of the sediment volume at initial heights of 10 cm and 4 m. The resulting plots shown in Figure 10.2 illustrate that small-scale laboratory experiments reach the fully settled configuration faster than plant-scale vessels. This can be explained by considering that the total distance the particles must travel to reach the full sediment configuration at plant scale is larger than the lab-scale experiments.



a) initial interface height is  $z_0 = 10$  cm; initial solids concentration of the suspended sample is  $\phi = \frac{\phi_{\max}}{4}$



b) initial interface height is  $z_0 = 4$  m; initial solids concentration of the suspended sample is  $\phi = \frac{\phi_{\max}}{4}$

**Figure 10.2.** Predicted Sedimentation Curves for Various Waste Types at Different Scales

## 11.0 Shear Strength Model

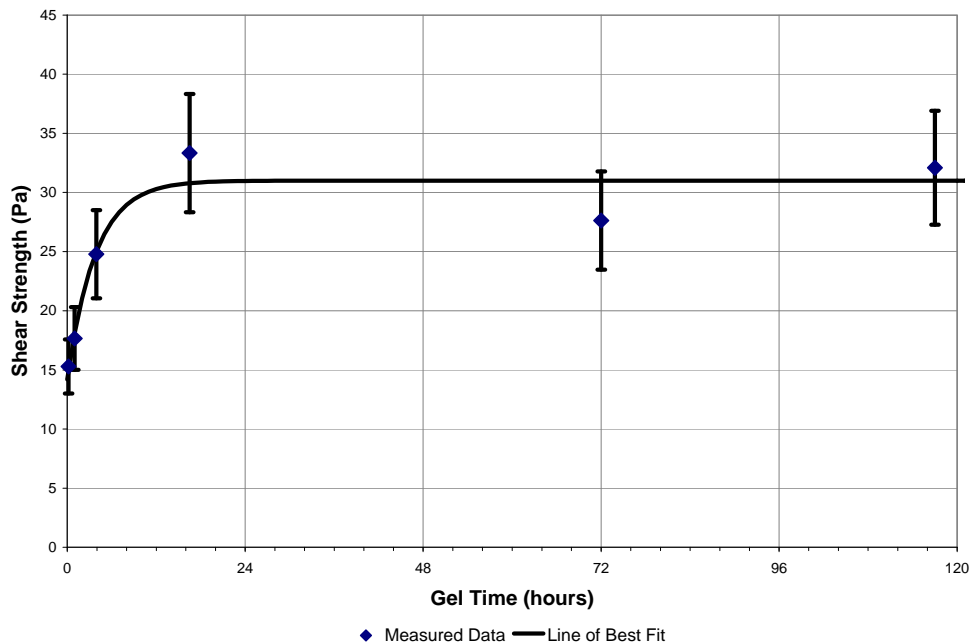
Shear strength is a transient property that grows during the time a sample remains quiescent. A model describing the growth of shear strength with respect to time is presented by Speers et al. (1987), who describe the shear strength rebuild behavior for several drilling mud slurries with a first-order rate model:

$$\frac{G_t - G_\infty}{G_0 - G_\infty} = e^{-kt} \quad (11.1)$$

where

- $G_t$  = shear strength
- $t$  = gel time
- $G_0$  = initial shear strength
- $G_\infty$  = equilibrium shear strength
- $k$  = gel time constant.

Only limited data were available for shear strength as a function of gelation time, but this model appears to be a good fit to the AZ-101 pretreated sludge shear-strength data (Poloski et al. 2003b) shown in Figure 11.1. The model-fit parameters observed for the AZ-101 pretreated sludge are reported in Table 11.1. Using this model, the initial shear-strength parameter (14.2 Pa) should roughly agree with the measured rheological Bingham-yield-stress measurement (14.7 to 18.1 Pa) (Poloski et al. 2003b). This model indicates that the shear strength rebuilds immediately from the time that it remains unshared. The material is expected to reach 95% of its steady-state shear strength (31 Pa) 9 hours from this time.



**Figure 11.1.** Shear Strength as a Function of Gel Time for HLW Pretreated Sludge

**Table 11.1.** Shear Strength Model Fit Parameters for Pretreated AZ-101 Sludge

Variable	Model Fit
$G_t$	See Figure 11.1 ( $r^2=0.929$ )
t	0 to 120 hours
$G_0$	14.2 Pa.
$G_\infty$	31 Pa
k	0.262 hr <sup>-1</sup>

These AZ-101 pretreated sludge shear strength data represent the only transient shear strength data found for Hanford waste suspensions. While other data exists to estimate the initial and steady-state shear strength values for several tank wastes, the only source for the gel time constant describing how quickly the shear strength rises to its steady state value is from AZ-101 pretreated sludge. A comparison of the AZ-101 pretreated sludge gel time constant against other suspensions either used in industry or for Hanford simulants is shown in Table 11.2. These data illustrate that the measured time constant of 0.262 hr<sup>-1</sup>, while high, is comparable with other fine particulate slurry systems. A graphical view of the time it takes to reach 95% of the growth in shear strength for these systems is shown in Figure 11.2. The numbers closes to the x-axis are the temperature in °C at which these shear strengths were measured. This figure portrays that the AZ-101 pretreated sludge material nearly reaches the equilibrium shear strength in approximately 10 hrs.

In the absence of actual shear strength as a function of time data, the transient shear strength model can be approximated through the following equation:

$$\frac{G_t - \tau_\infty}{\tau_0^B - \tau_\infty} \cong e^{-kt} \quad (11.2)$$

where

$G_t$  = shear strength

t = the gel time

$\tau_0^B$  = the Bingham yield stress

$\tau_\infty$  = the single point equilibrium shear strength measurement

k = the gel time constant.

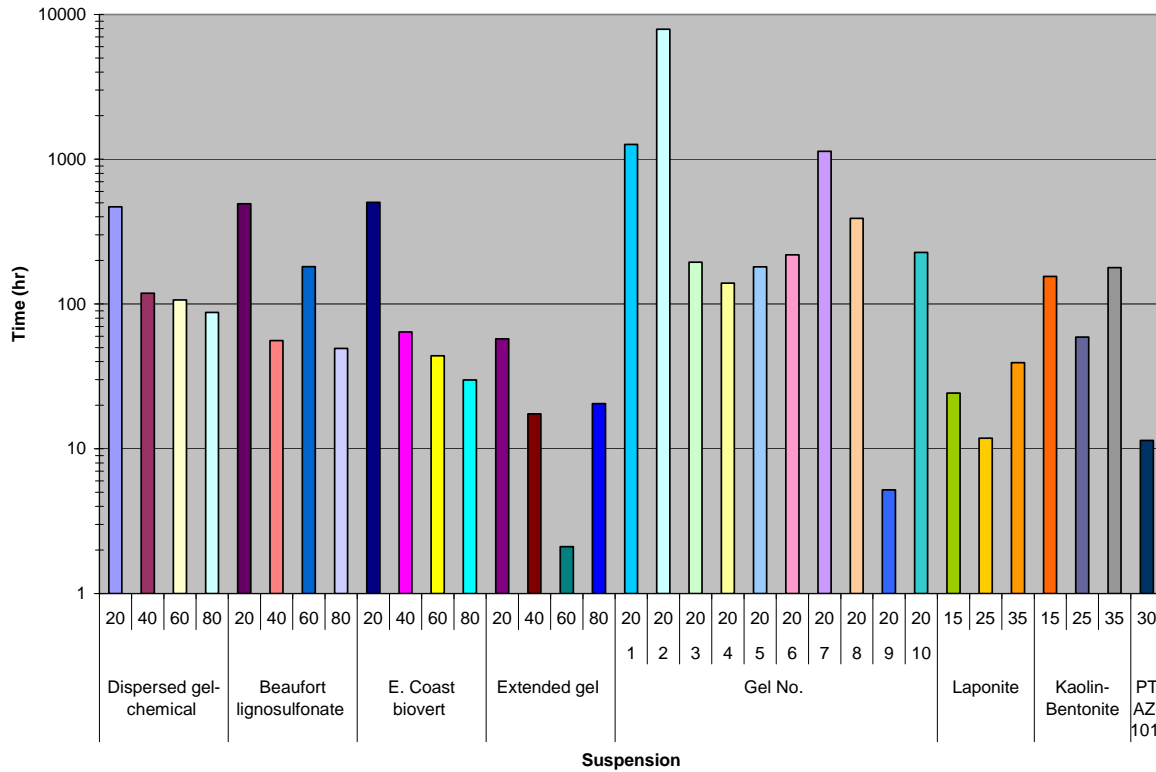
In this model, the initial shear strength is replaced by the Bingham Plastic yield stress,  $\tau_0^B$ , while the equilibrium shear strength is approximated by a single point shear strength measurement,  $\tau_\infty$ , because most shear strength measurements were taken after the sample sat undisturbed for several days. Currently, a gel time constant of 0.262 hr<sup>-1</sup> is used based on the fit for the pretreated AZ-101 sludge. Until additional transient shear strength data are obtained, this gel time constant is recommended for Hanford tank waste.

**Table 11.2.** Shear Strength Rebuild Parameters for Various Materials

Material	Temperature (°C)	Initial Shear Strength, $G_0$ (Pa)	Gel Time Constant, $k$ (hr <sup>-1</sup> )	Steady-State Gel Strength, $G_\infty$ (Pa)	Correlation Coefficient ( $r^2$ )	
Dispersed gel-chemical <sup>(a)</sup>	20	2.4	0.00637	14.0	0.96	
	40	2.2	0.0253	4.7	0.986	
	60	1.8	0.028	4.2	0.985	
	80	1.8	0.0342	4.3	0.993	
Beaufort lignosulfonate <sup>(a)</sup>	20	5.0	0.00609	16.5	0.908	
	40	1.6	0.0535	3.1	0.924	
	60	1.6	0.0165	4.8	0.933	
	80	1.4	0.0607	3.8	0.964	
E. Coast biovert <sup>(a)</sup>	20	2.7	0.00595	14.1	0.95	
	40	1.5	0.0467	7.8	0.991	
	60	1.7	0.0681	9.7	0.986	
	80	2.0	0.1	11.8	0.996	
Extended gel <sup>(a)</sup>	20	5.8	0.0522	10.9	0.932	
	40	5.2	0.172	8.0	0.977	
	60	3.9	1.42	4.9	0.923	
	80	2.7	0.146	3.9	0.956	
Gel <sup>(a)</sup> no	#1	20	2.5	0.00237	16.6	0.962
	#2	20	8.1	0.000378	16.6	0.956
	#3	20	1.8	0.0154	15.0	0.986
	#4	20	13.7	0.0215	24.5	0.981
	#5	20	1.1	0.0166	13.6	0.99
	#6	20	13.5	0.0137	34.0	0.958
	#7	20	1.2	0.00264	14.3	0.958
	#8	20	4.5	0.00767	16.0	0.93
	#9	20	5.2	0.576	10.6	0.954
	#10	20	3.1	0.0132	14.2	0.913
Laponite PJM Simulant <sup>(b)</sup>	15	79.5	0.123	141.4	0.866	
	25	63.6	0.254	139.8	0.922	
	35	71.1	0.0761	149.7	0.995	
Kaolin-Bentonite PJM Simulant <sup>(b)</sup>	15	36.4	0.0193	70.0	0.916	
	25	41.4	0.0506	74.7	0.964	
	35	48.4	0.0168	97.2	0.905	
AZ-101 Pretreated (PT) Sludge <sup>(c)</sup>	30	14.2	0.262	31	0.929	
(a) Speers et al. (1987).						
(b) Poloski et al. (2004).						
(c) Poloski et al. (2003b).						

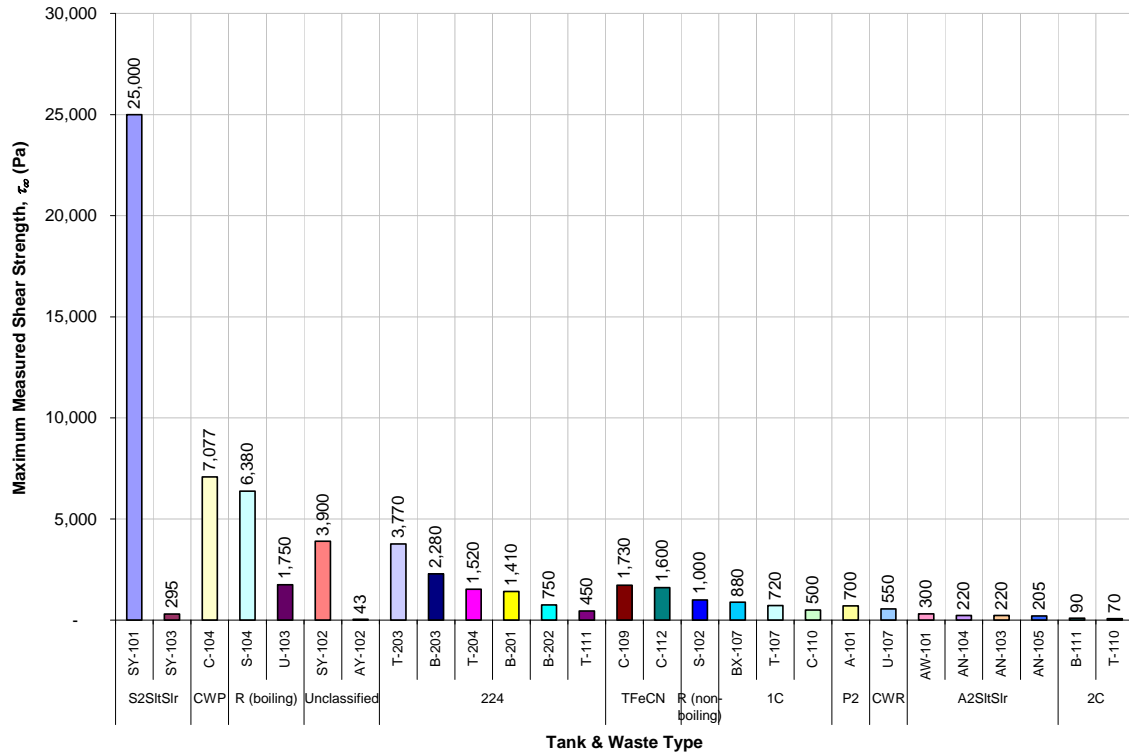
Values for the single point equilibrium shear strength,  $\tau_\infty$ , are provided in Figure 11.3. Falling ball rheometer and shear vane measurements were compiled, and the maximum measured value for each tank is shown in Figure 11.3. A breakdown of the primary sludge waste type is also provided. Saltcake waste

types are stated in the absence of a sludge waste type. The gaps in the waste types represented in this shear strength data are shown in Figure 11.4. The relative volume of each waste type in the tanks where shear strength data was analyzed (red bar in the front of the graph) is compared to the total volume of waste associated with those waste types (blue bar in the back of the graph). Saltcake waste types are stated in the absence of a sludge waste type.

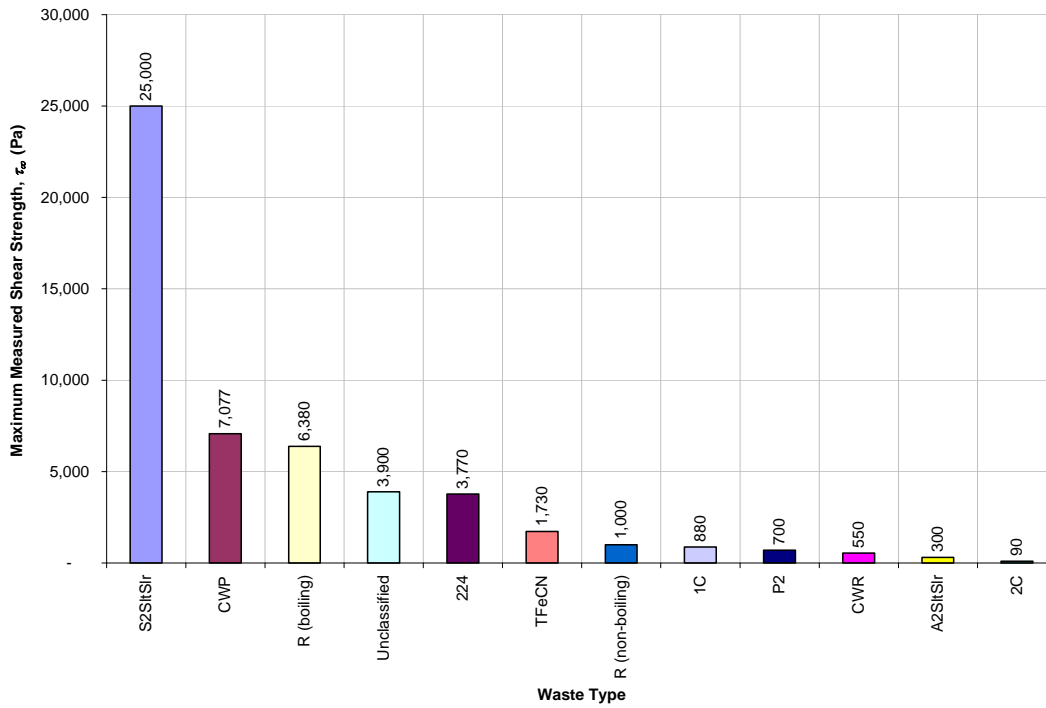


**Figure 11.2.** Gel Time Constant Comparison of Various Particulate Suspensions and Temperatures (°C)

An analysis of the slurry composition for the tanks identified with maximum shear strength for each waste type was performed. The analysis reveals that, with the exception of the saltcake wastes, shear strength increases with increasing concentration of the following species (in order of significance) zirconium compounds > boehmite > bismuth compounds > gibbsite > iron hydroxide. Silica and aluminosilicate content did not show a strong effect on shear strength.



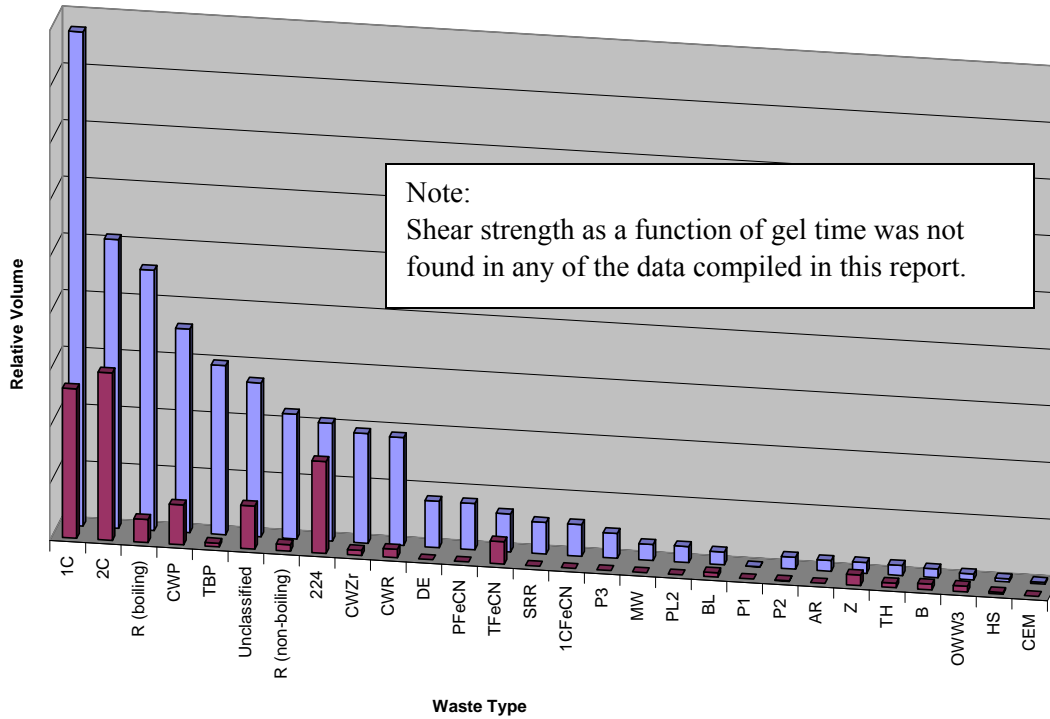
a) Maximum measured shear strength for each Hanford waste tank



b) Maximum measured shear strength for each Hanford waste type

**Figure 11.3.** Shear Strength Summary for Various Hanford Waste Tanks and Types





**Figure 11.4.** Gaps in Data Available for Shear Strength Modeling as a Function of Waste Type

This observation can be explained by a particle size argument. The zirconium compounds, boehmite, bismuth compounds, gibbsite, and iron hydroxide particles are generally submicron, colloidal particles with a large surface-to-mass ratio (Wells et al. 2007). The silica present in the tank waste is generally thought to come from Hanford sand with a much larger particle size (Wells et al. 2007). Zhou and coworkers (2001) present an equation that states at a given surface chemistry condition the shear strength of a non-Newtonian fluid varies according to:

$$\tau_{\infty} = \frac{K}{d^2} \phi^c \quad (11.3)$$

where

- $K$  = a constant which relates bond strength to material properties and surface chemistry condition
- $d$  = the particle diameter
- $c$  = a fitting parameter.

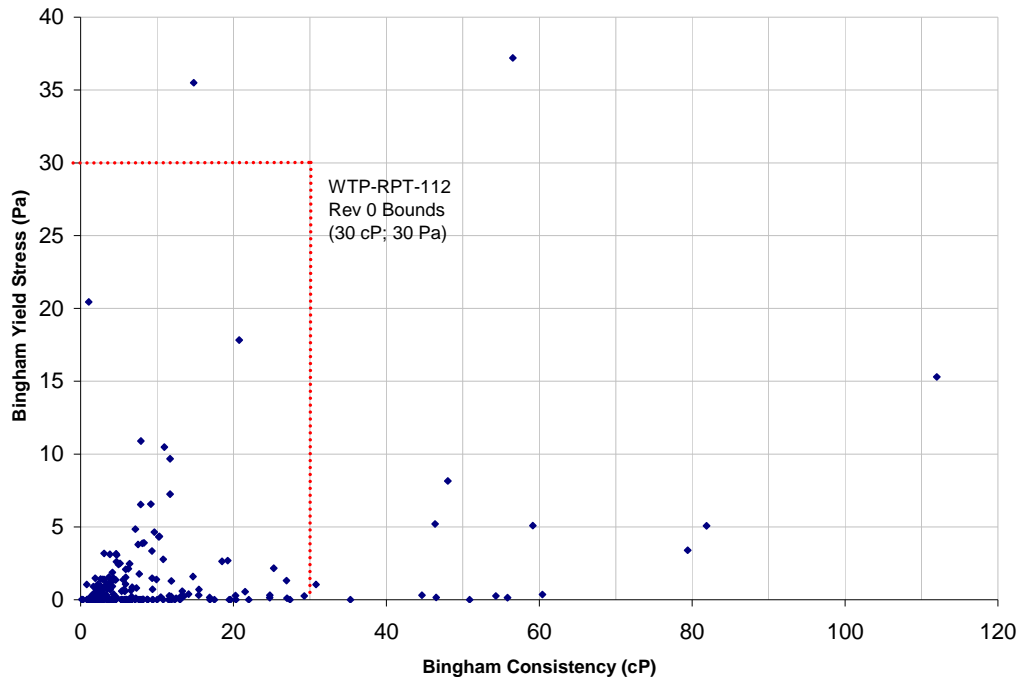
In this situation, increases in the relative amounts of  $ZrO_2$ , boehmite, gibbsite, and iron hydroxide would reduce the overall particle diameter and increase shear strength. Adding silica would raise the particle diameter and reduce shear strength of the mixture. Bingham yield stress,  $\tau_0^B$ , can also be modeled with an equation of the same form as Eq. (11.3).

Saltcake waste had the largest measured shear strength, which is attributed to precipitated salt bridges between particles. It is unclear whether saltcake shear strength is reversible (will rebuild to these high levels). These bridges will likely require excessive time or a change in chemical composition to reform.

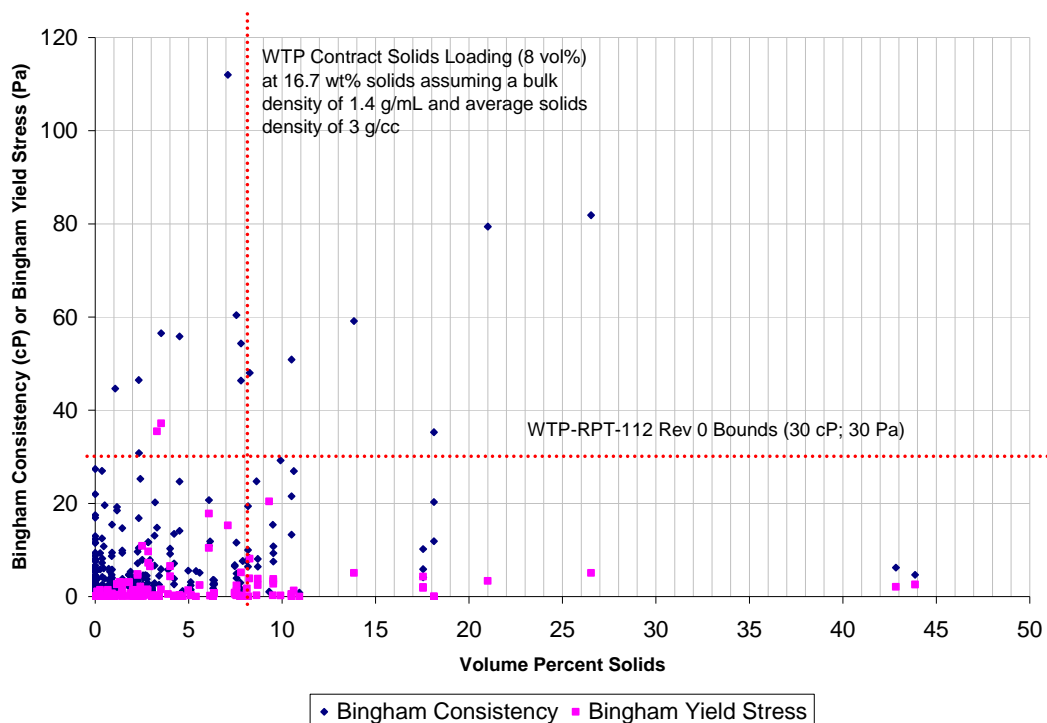
## 12.0 Bingham Plastic Modeling

Hanford slurries can be characterized rheologically as non-Newtonian, Bingham plastic fluids. Bingham plastic model fits for 28 waste tanks from 12 sludge types covering a range of temperatures from 20° to 95°C were obtained from the available literature. Figure 12.1 shows the range of Bingham parameters (Bingham consistency and yield stress) from approximately 300 flow curves. For reference, the HLW pretreated sludge boundaries discussed by Poloski and coworkers (2006a) are also placed on the figure. These data indicate that the Hanford tank feed has a greater tendency for exceeding the 30 cP Bingham consistency parameter (15 measurements) than the Bingham yield stress (3 measurements). Only two measurements exceeded both the yield stress and consistency boundaries.

The Bingham plastic rheological parameters are a strong function of the undissolved solids loading. Figure 12.2 shows how the Bingham plastic parameters vary with undissolved solids concentration. Again, the HLW pretreated sludge rheological bounds discussed by Poloski et al. (2006a; WTP-RPT-112 Rev 0) are shown in the figure. In addition, the WTP contract solids processing specification of 16.7 wt% solids has been converted to an estimate of volume percent undissolved solids to provide a process throughput reference point. Data points in the lower right quadrant should have moderate rheology while meeting or exceeding contract throughput specifications. The lower left quadrant identifies slurries with moderate rheology that are within contract throughput specifications. The upper right quadrant identifies slurries with high rheology where further dilution is likely needed to lower slurry rheological properties and meet contract throughput specifications. The upper left quadrant identifies slurries with high rheology, where further dilution may lead to moderate rheology while meeting throughput specifications.



**Figure 12.1.** Scatter Plot Showing the Range of Measured Bingham Parameters



**Figure 12.2.** Scatter Plot of Obtained Bingham Parameters at Various Solids Loadings

While single points are shown on the scatter plot, each point actually lies on a series of dilution curves. Because of the exponential nature of rheological properties with respect to solids concentration, a small dilution can drastically lower the rheological properties of a fluid. Therefore, the high rheological point at 80 cP consistency and 27 Pa yield stress should not be considered an anomaly. This data point demonstrates the extreme rheology for this class of material achievable from concentrating solids from a slurry.

Several of the data points in Figure 12.2 are for the same tank sample diluted with water to various solid contents. To gain an understanding of how the rheological parameters in the database vary by Hanford waste tank and waste type, Figures 12.3 and 12.4 were created based on the maximum measured Bingham parameters for each waste tank. Figure 12.3 illustrates that R-(boiling), TFeCN, saltcake, and 224 wastes tend to exhibit high Bingham consistency values; Figure 12.4 shows that TFeCN, R-(boiling), 224, and CWP wastes exhibit relatively high Bingham yield stress values.

Interestingly, TFeCN, R-(boiling), 224, and CWP wastes also appear to be among the wastes with the large measured shear strength values. Consequently, these waste types appear to have the largest degree of non-Newtonian behavior. Because these wastes tend to be relatively high in iron hydroxide, boehmite, aluminosilicate, zirconium compounds, and bismuth compounds, the trend observed between solids composition and shear strength appears to be applicable to flow curve behavior also.

While saltcake wastes have among the highest Bingham consistency values, they have moderate Bingham yield stress values. Again, this supports the hypothesis that the high shear strength for the saltcake wastes is a nonreversible artifact of salt bridging between particles. Once these salt bridges are broken the yield stress reduces to moderate levels.

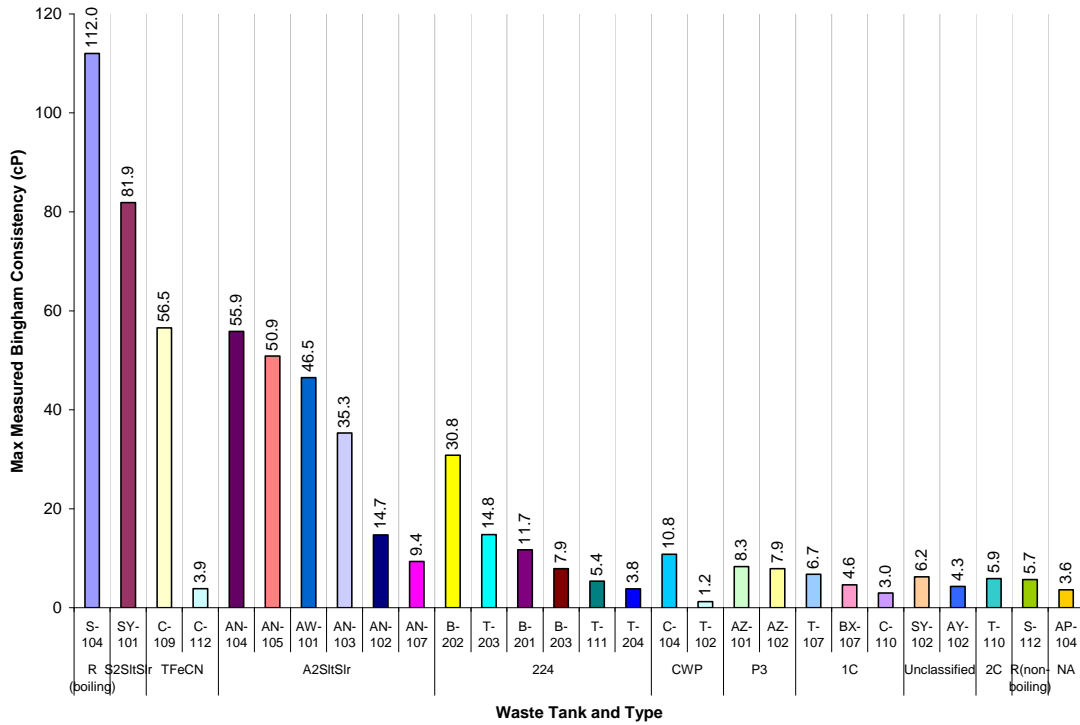


Figure 12.3. Maximum Measured Bingham Consistency for Various Hanford Tanks and Waste Types

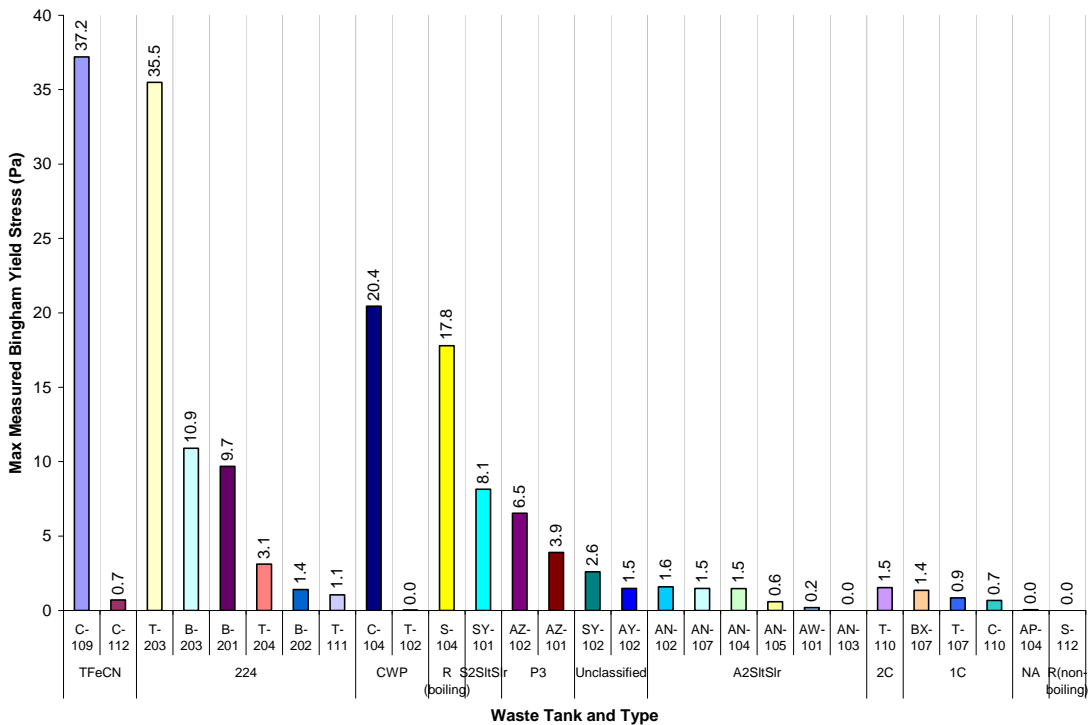


Figure 12.4. Maximum Measured Bingham Yield Stress for Various Hanford Tanks and Waste Types

Ferraris and co-workers (2001) provide an equation that describes how the Bingham plastic consistency parameter varies with solids concentration:

$$\eta_P = ae^{b\phi} \quad (12.1)$$

where

- $\eta_P$  = the Bingham consistency in cP
- $\phi$  = the solids volume fraction
- $a$  and  $b$  = fitting parameters.

Zhou and coworkers (2001) provide an equation that describes how the Bingham yield stress varies with solids concentration (Eq. 12.2). This equation is of similar form to the shear strength equation.

$$\tau_o^B = c\phi^d \quad (12.2)$$

where

- $\tau_o^B$  = the Bingham yield stress
- $\phi$  = the solids volume fraction
- $c$  and  $d$  = fitting parameters.

These equations are typically valid only when the chemistry of the slurry is held constant while varying the solids loading. This can be achieved by diluting the slurry with decanted or separated interstitial liquid which is at equilibrium with the slurry solids. Unfortunately, this protocol was not observed and water was used as a diluent in all of the dilution studies cited in this report. Nonetheless, the data compiled in this report was modeled using Eq. (12.2) and (12.3) to find a correlation between rheological parameters and solids concentration.

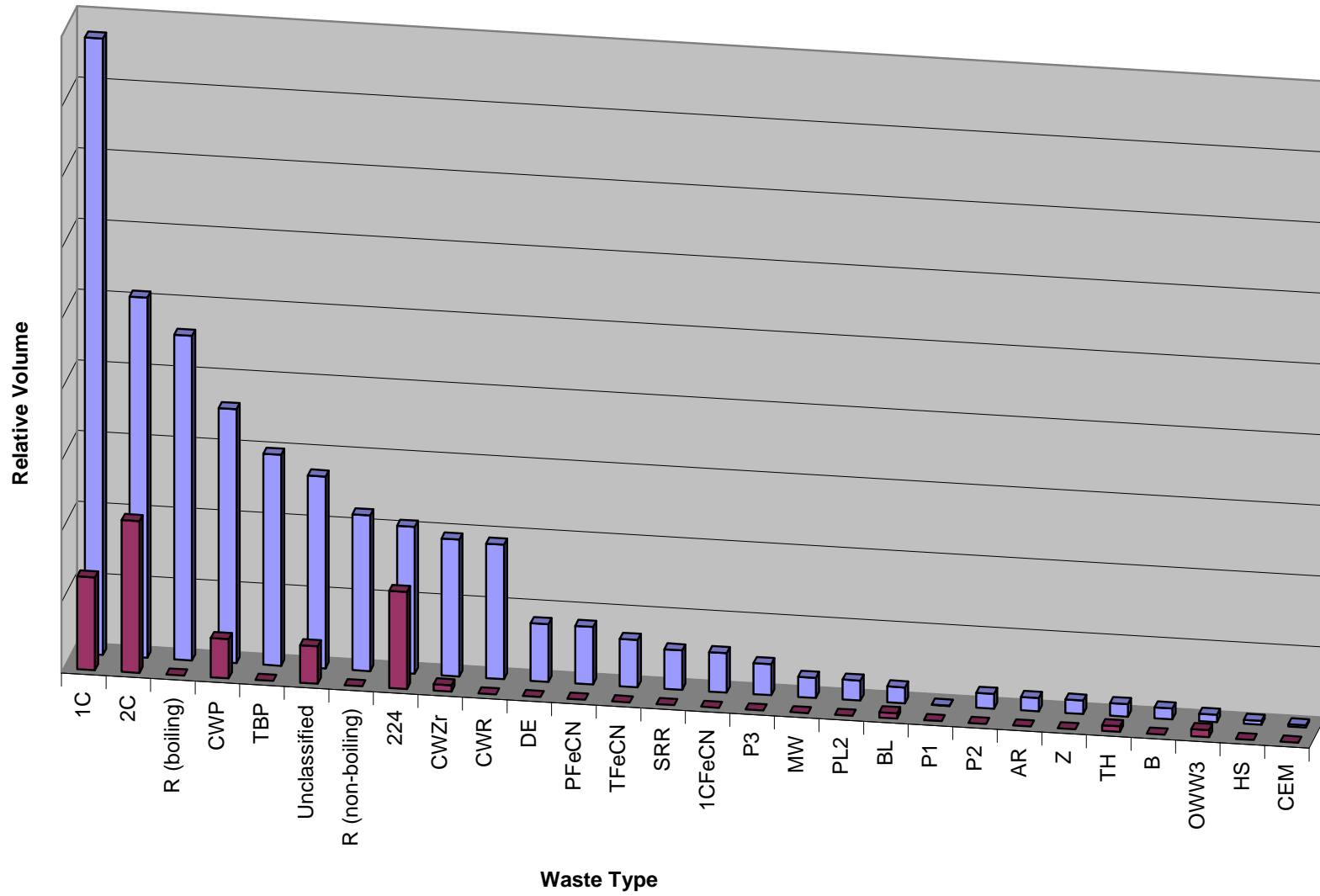
Several correlations were found that had correlation coefficients ( $r^2$ ) above 0.7, 17 correlations were found for Bingham consistency and 10 correlations for Bingham yield stress. These data cover eight Hanford waste tanks, with five waste types represented including 224, 1C, 2C, A2Sltslr, and CWP. The parameters for these correlations are shown in Table 12.1. Gaps in waste types used in these rheological correlations are shown in Figure 12.5. Several of these correlations indicate that relatively high rheological parameters (>30 cp or 30 Pa) exist at low solids concentrations (>8 vol% undissolved solids). These fluids may pose throughput challenges to the WTP as additional dilution may be required to achieve moderate rheological parameters.

Plots presenting the raw data used to evaluate these correlations are shown in Appendix B, while plots of the data and correlations can be found in Appendix C. Example plots showing a good correlation with Eq. (12.2) and (12.3) are shown in Figures 12.6 and 12.7. Figure 12.6 shows the relationship between C-104 as-received tank core samples and solids concentration, while Figure 12.7 shows the same relationship for the water-diluted C-104 core samples. These data are a combination of tank core sample characterization reports and cross-flow filtration studies. A peak in the yield stress trend and minimum in the consistency trend are observed in this figure.

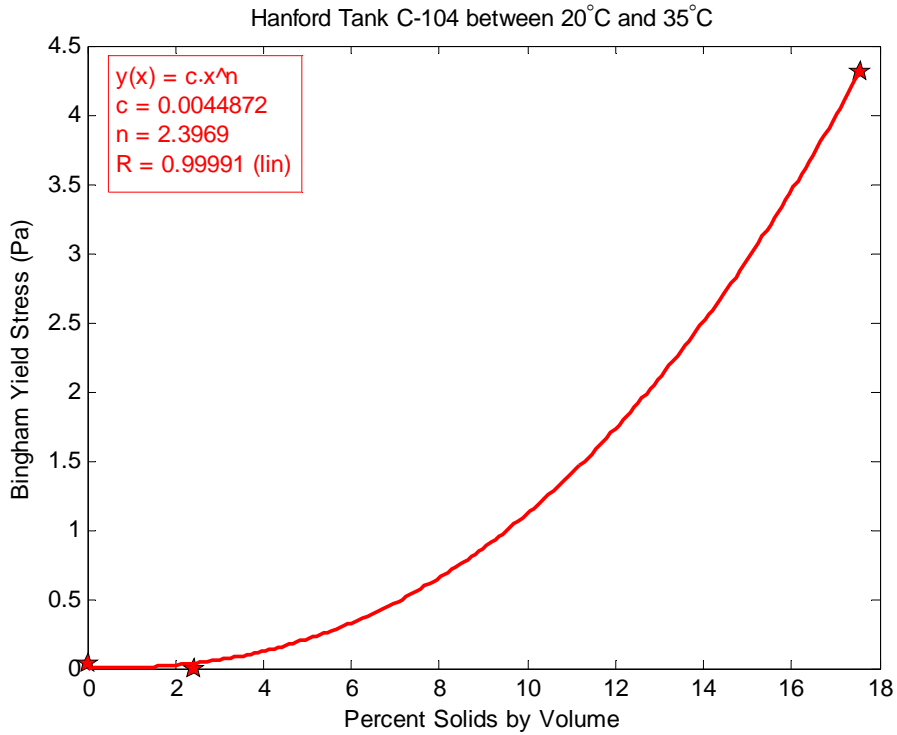
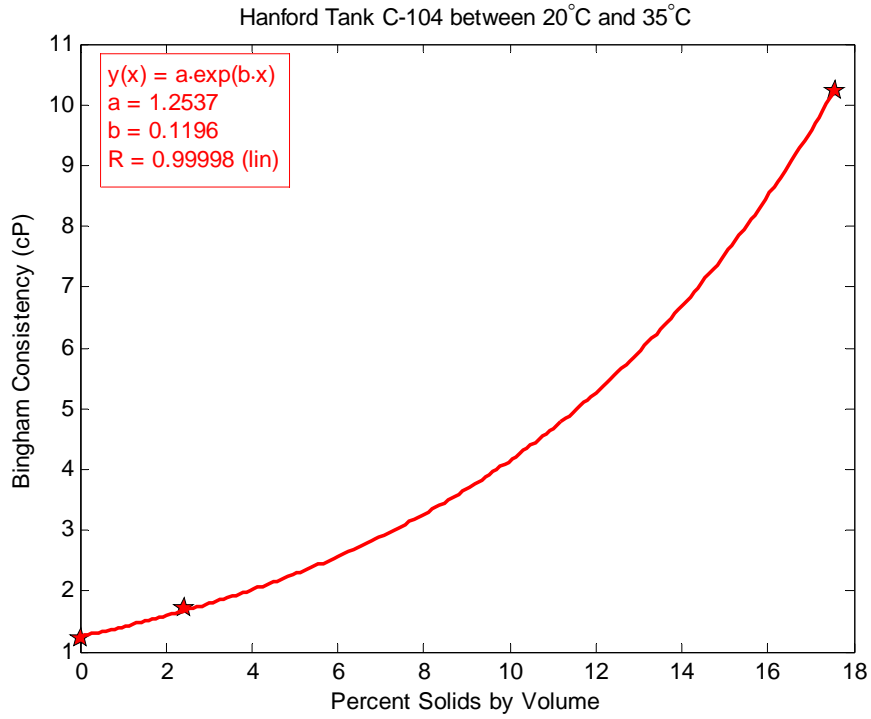
**Table 12.1.** Bingham Model Parameters for Various Hanford Tanks

Waste Type	Waste Tank	Waste Status	Temperature Category (°C)	Consistency Parameter, <i>a</i> (cP)	Consistency Parameter, <i>b</i> (-)	Consistency Model Correlation Coefficient, <i>r</i> <sup>2</sup>	Predicted Solids Loading at 30 cP Consistency (vol%)	Yield Stress Parameter, <i>c</i> (Pa)	Yield Stress Parameter, <i>d</i> (-)	Yield Stress Model Correlation Coefficient <i>r</i> <sup>2</sup>	Predicted Solids Loading at 30 Pa Yield Stress (vol%)
224	B-202	Washed	20-35	1.51	36	0.91	8.3	7.21E+04	2.94	0.95	7.1
224	B-203	Washed	20-35	1.30	72	1.00	4.4	1.31E+07	3.80	1.00	3.3
224	T-111	Washed	20-35	2.64	37	0.82	6.5	n/r	n/r	n/r	n/r
224	T-203	Washed	20-35	1.08	79	1.00	4.2	2.50E+05	2.60	1.00	3.1
224	B-202	Washed	80-95	1.01	40	0.71	8.5	2.34E+04	2.62	0.92	7.9
224	T-111	Washed	80-95	1.16	43	0.90	7.6	n/r	n/r	n/r	n/r
1C	BX-107	Washed	20-35	1.64	37	0.98	7.9	n/r	n/r	n/r	n/r
<i>1C</i>	<i>BX-107</i>	<i>Washed</i>	<i>80-95</i>	<i>0.97</i>	<i>54</i>	<i>0.92</i>	<i>6.3</i>	<i>1.28E+15</i>	<i>9.53</i>	<i>1.00</i>	<i>3.7</i>
<i>2C</i>	<i>T-110</i>	<i>Washed</i>	<i>20-35</i>	<i>1.16</i>	<i>46</i>	<i>1.00</i>	<i>7.0</i>	<i>1.21E+04</i>	<i>2.68</i>	<i>1.00</i>	<i>10.7</i>
A2SlrSlr	AN-105	Salt Cake	20-35	1.38	34	0.95	9.0	n/r	n/r	n/r	n/r
A2SlrSlr	AN-105	Salt Cake	35-50	3.37	17	0.93	13.0	n/r	n/r	n/r	n/r
A2SlrSlr	AN-105	Salt Cake	50-65	1.83	18	0.95	15.3	n/r	n/r	n/r	n/r
A2SlrSlr	AN-104	Washed	20-35	11.35	35	0.87	2.8	n/r	n/r	n/r	n/r
A2SlrSlr	AN-104	Washed	35-50	7.53	26	0.91	5.3	n/r	n/r	n/r	n/r
A2SlrSlr	AN-104	Washed	50-65	4.83	24	0.92	7.7	n/r	n/r	n/r	n/r
CWP	C-104	Salt Cake	20-35	1.25	12	1.00	26.5	2.79E+02	2.40	1.00	39.4
CWP	C-104	Washed	20-35	0.78	28	1.00	13.2	4.13E+03	3.11	1.00	20.5
CWP	C-104	Washed	35-50	0.45	32	0.99	13.3	1.59E+04	3.60	1.00	17.5
CWP	C-104	Washed	50-65	0.36	32	0.99	13.9	4.90E+04	4.03	1.00	15.9
<i>S2SlrSlr</i>	<i>SY-101</i>	<i>Salt Cake</i>	<i>20-35</i>	<i>43.05</i>	<i>3.7</i>	<i>0.91</i>	<i>0</i>	<i>n/r</i>	<i>n/r</i>	<i>n/r</i>	<i>n/r</i>
S2SlrSlr	SY-101	Salt Cake	35-50	16.47	6.4	0.95	9.4	7.14E+01	1.98	0.99	64.6
S2SlrSlr	SY-101	Salt Cake	65-80	8.32	14	0.76	9.0	1.19E+02	1.58	0.65	41.9
<i>S2SlrSlr</i>	<i>SY-101</i>	<i>Salt Cake</i>	<i>80-95</i>	<i>16.18</i>	<i>13</i>	<i>1.00</i>	<i>4.7</i>	<i>n/r</i>	<i>n/r</i>	<i>n/r</i>	<i>n/r</i>
Unclassified	AY-102	Salt Cake	50-65	0.80	6.8	0.46	52.9	n/r	n/r	n/r	n/r

n/r – not reported due to poor correlation results  
*italics* – predicted to achieve relatively large rheological parameters at low solids concentrations.



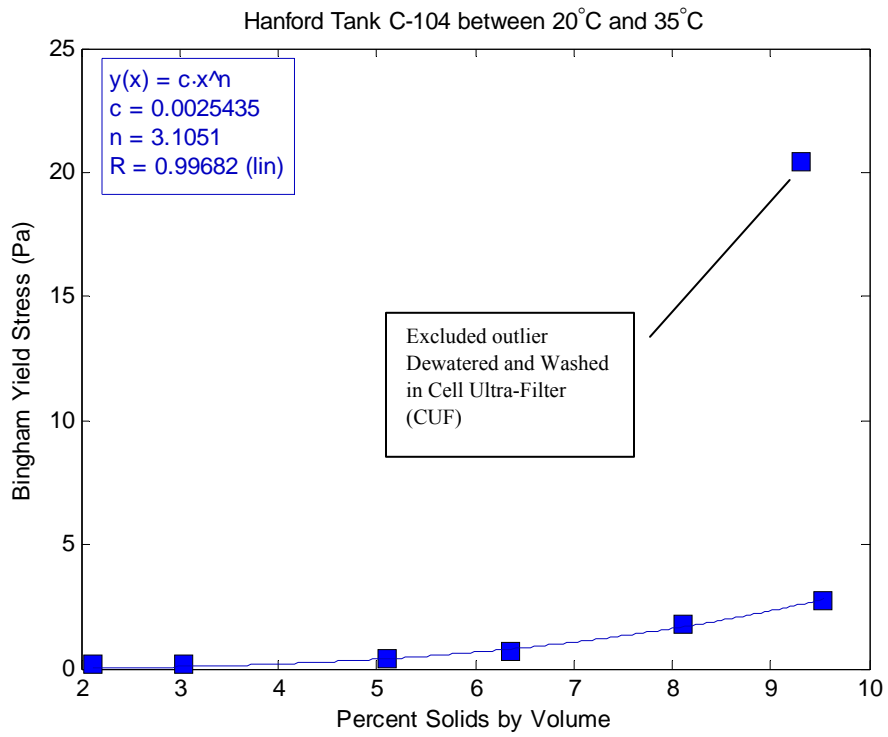
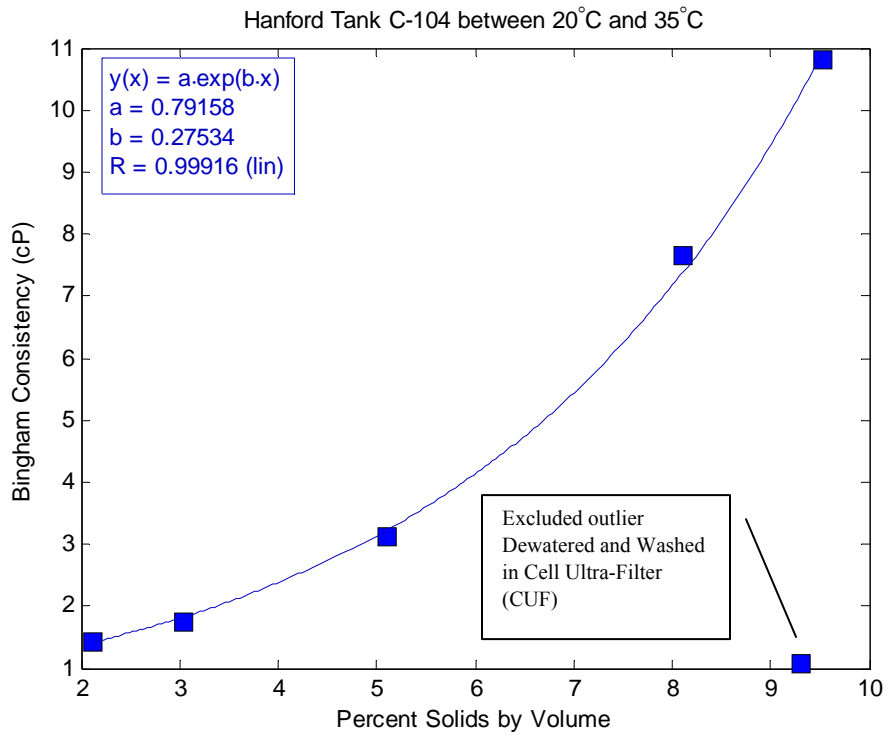
**Figure 12.5.** Gaps in Data Available for Rheological Correlations as a Function of Waste Type



Stars = as-received tank waste

**Figure 12.6.** Bingham Plastic Rheological Parameters as a Function of Solids Loading for Tank C-104 as an Example of an as-Received Hanford Core Sample





Squares represent water added as diluent

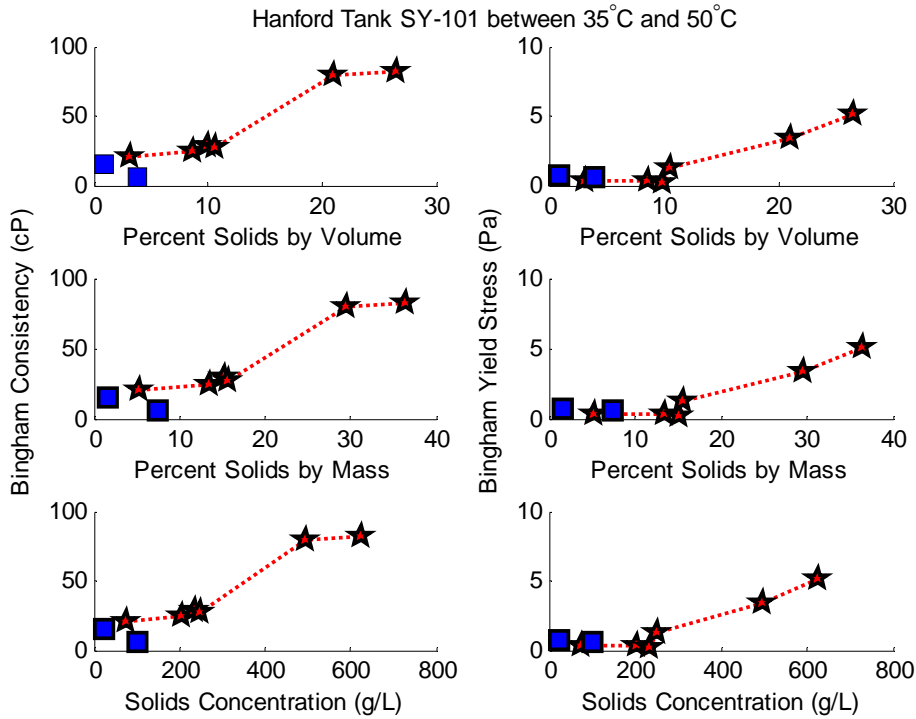
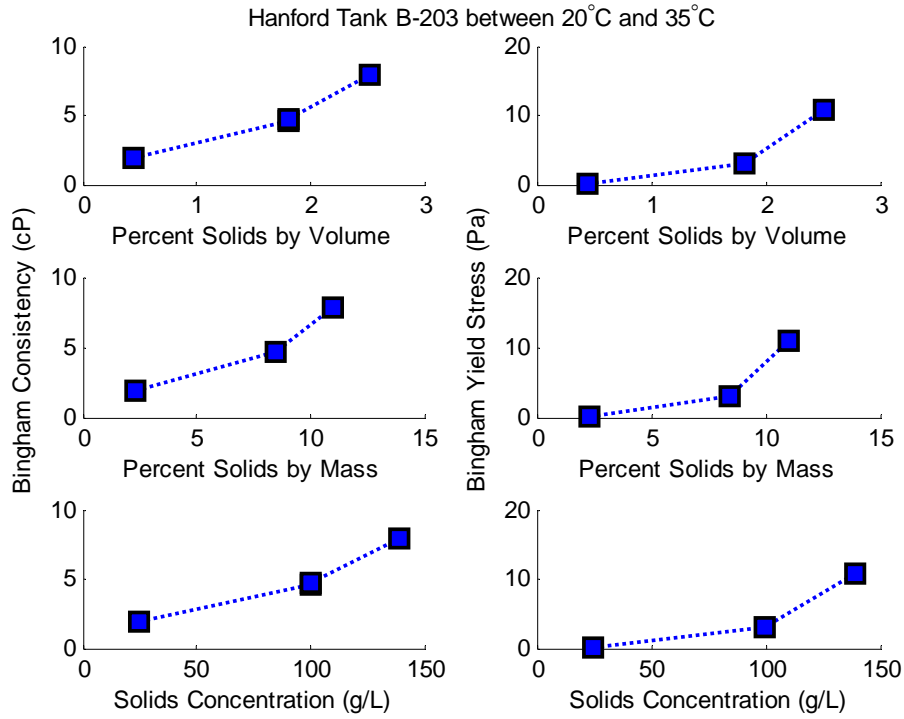
**Figure 12.7.** Bingham Plastic Rheological Parameters as a Function of Solids Loading for Tank C-104 as an Example of a Hanford Core Sample Diluted with Water

This peak shows the import of sample process history as it corresponds to a sample that was processed in the cell ultra-filter. The sample underwent similar chemical changes as it was dewatered and water washed to a certain solids loading. However, the use of the filtration equipment may have altered the slurry physical properties through dissolution of salt cake particles, a lowered ionic strength (zeta potential), and potential particle attrition from the pump/filter loop. For this reason, the point was discarded from the correlation analysis but kept in the above analysis on maximum rheological values as sample process history will vary widely from tank retrieval through vitrification. A more detailed look at the affect of WTP pretreatment process operations on rheological properties is needed to gain confidence in the current process design.

Example plots from Appendix B have been selected to illustrate two important observations made while preparing this report. These plots are shown in Figures 12.8 and 12.9. Figure 12.8 shows the expected “mechanically dominated” dilution behavior where rheological properties exponentially decrease with water dilution due to the simple reduction of particle/particle interactions.

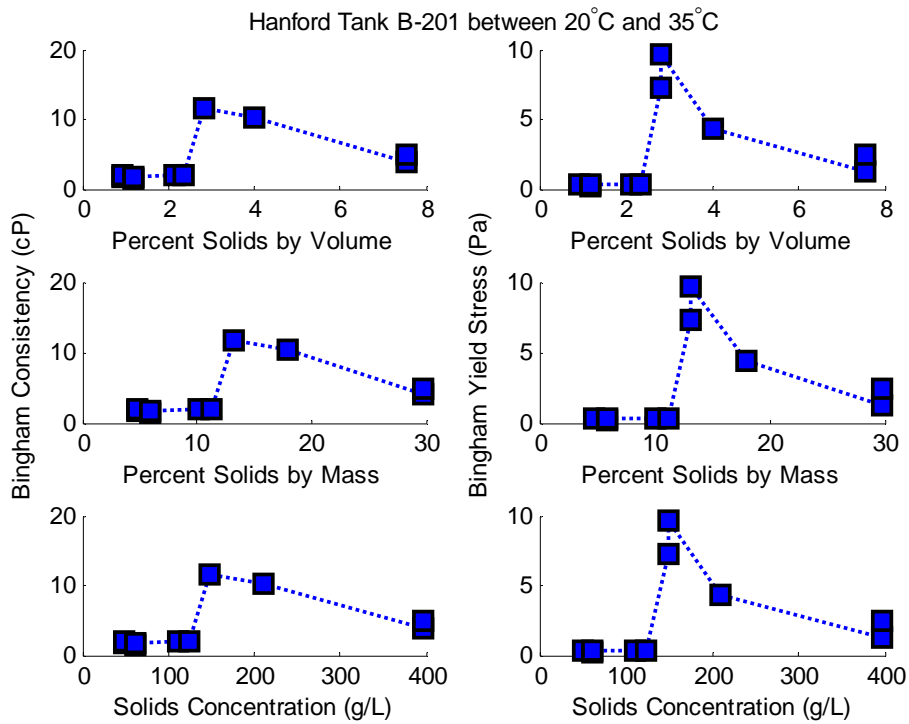
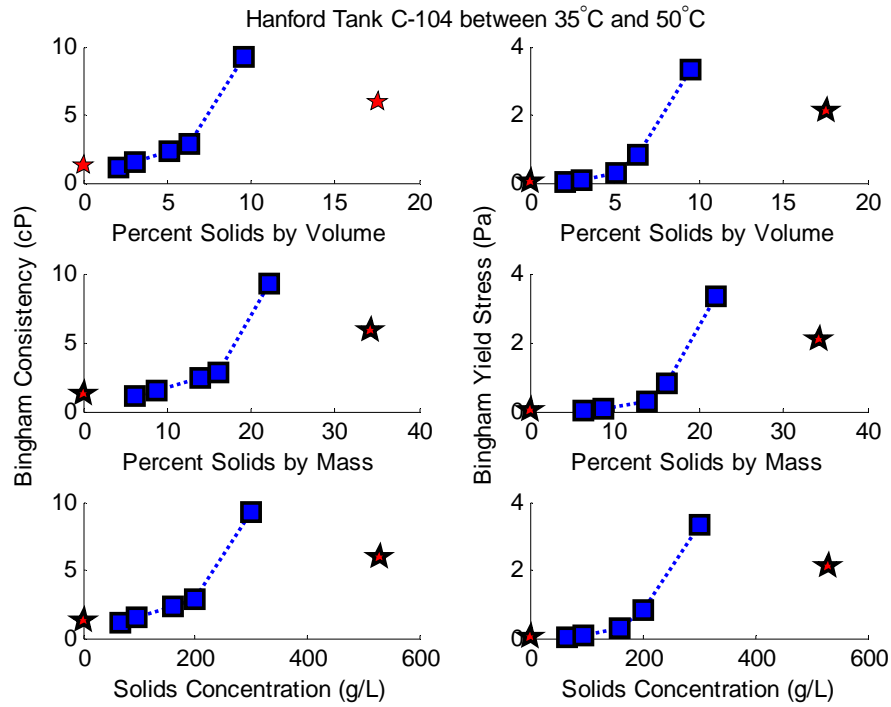
In reality, the parameters  $a$ ,  $b$ ,  $c$ , and  $d$  from Eq. (12.2) and (12.3) can vary significantly with slurry chemical and physical properties such as zeta potential, particle size, particle chemistry, and aqueous chemistry. As dilution with water occurs, all of these properties are likely to vary as salt particles dissolve changing average particle size and chemistry, aqueous species are diluted while salt species are added, and solution equilibrium is achieved. The fact that the expected “mechanical” trend is maintained during this process indicates that the effect of these changes is minimal and the slurry rheology is dominated by mechanical forces.

On the other hand, Figure 12.9 shows “chemically dominated” dilution behavior where rheological properties actually increase to a maximum value with water dilution. In this scenario, as the sample is diluted with water, chemical properties vary as salt particles dissolve. This changes average particle size, particle chemistry, aqueous speciation, and interaction potentials as a new solution equilibrium is achieved. Saltcake solids are typically on the order of several tens or hundreds of micrometers, while sludge particles are on the order of ten micrometers or smaller (Wells et al. 2007). The shift to smaller particle size,  $d$ , alone will result in a peak with regards to yield stress as the parameter,  $c \propto d^2$  (Zhou et al. 2001). Additionally, dilution will ultimately result in a reduction in solution ionic strength and zeta potential. The parameter  $c$  will reach a maximum value when the zeta potential is zero (Zhou et al. 2001). Consequently, in some cases, dilution with water will result in a rheological maximum due to these surface chemistry effects. Several additional examples of “mechanically dominated” and “chemically dominated” dilution phenomena can be seen in Appendix B.



Stars = as-received tank waste; squares = water added as diluent

**Figure 12.8.** Bingham Plastic Rheological Parameters as a Function of Solids Loading for a Water-Diluted Hanford Core Sample Showing Decreasing Rheology as Dilution Occurs



Stars = as-received tank waste; squares = water added as diluent

**Figure 12.9.** Bingham Plastic Rheological Parameters as a Function of Solids Loading for a Water-Diluted Hanford Core Sample Showing a Rheological Peak as Dilution Occurs

## 13.0 Transient Modeling

During off-normal events, the WTP processing system may lose power and become inoperable. In these situations, the slurries will remain quiescent for some time until backup/emergency systems are used or the primary system is restored. Understanding how rheological properties vary with time under quiescent conditions is an important design consideration. From the information presented above, an estimation of this transient rheological behavior can be obtained. The solids interface height of a sediment bed as a function of time (Renko 1996) in a sedimentation column was described in the sedimentation section of this report and shown as:

$$z(t, z_0) = \frac{C\phi_0 z_0}{\alpha} + \left( z_0 - \frac{C\phi_0 z_0}{\alpha} \right) e^{\frac{-\alpha}{\phi_0 z_0} t} \quad (13.1)$$

where

- $z$  = the interface height (m) at time  $t$  in hours
- $z_0$  = the initial interface height (m)
- $\phi_0$  = the initial solids concentration of the suspended sample (volume fraction)
- $\alpha$  and  $C$  = fitting parameters in  $\text{m/hr}^{-1}$ .

The solids concentration profile as a function of time was also presented by Renko (1998) and is shown as Eq. (13.2).

$$\phi(t, z) = \frac{\phi_0}{\frac{C\phi_0}{\alpha} + \left( 1 - \frac{C\phi_0}{\alpha} \right) \left( 1 - \frac{t\alpha}{\phi_0 z_0} \right) e^{\frac{-\alpha}{\phi_0 z_0} t}} \quad (13.2)$$

As sedimentation proceeds, the local Bingham consistency and yield parameter vary as a function of solids concentration. These equations were described in the Bingham plastic modeling section of this report and are shown as Eq. (13.3) and (13.4):

$$\eta_p = a e^{b\phi} \quad (13.3)$$

$$\tau_o^B = c \phi^d \quad (13.4)$$

where

- $\eta_p$  = Bingham consistency
- $\tau_o^B$  = Bingham yield stress
- $b, c, \text{ and } d$  = fitting parameters.

Shear strength as a function of time, for cohesive sludge layers that exclude frictional forces generated by coarse particles, was described in the shear strength modeling section of this report and is shown as

$$G_t = (\tau_O^B - \tau_\infty) e^{-kt_g} + \tau_\infty \quad (13.5)$$

where

$G_t$  = shear strength at any gel time

$\tau_\infty$  = single point equilibrium shear strength measurement

$\tau_O^B$  = Bingham yield stress

$t_g$  = gel time

$k$  = gel time constant ( $\text{hr}^{-1}$ ).

The equilibrium shear strength,  $\tau_\infty$ , (see Eq. 13.6) is assumed to have the same form and fitting parameter,  $d$ , as the correlation for Bingham yield stress (see Eq. 13.4). Consequently, if an equilibrium shear strength has been measured (due to the limited amount of Hanford waste data, a single point rather than an average is used for this calculation) at a given solids concentration,  $\phi$ , the fitting parameter  $c_\infty$  can be solved.

$$\tau_\infty = c_\infty \phi^d \quad (13.6)$$

Combining Eq. (13.1) through (13.6) allows one to predict solids concentration, Bingham consistency, Bingham yield stress, and shear strength as a function of time. However, Eq. (13.5) is only valid for a slurry in which the solids concentration remains constant (i.e., a fully settled slurry). Eq. (13.5) cannot be applied directly to an actively sedimenting slurry because both the gel structure and solids concentration are changing simultaneously. Additionally, if coarse particles are present in the sludge, frictional forces will be generated in addition to cohesive, interparticle forces. The frictional force contribution would need to be accounted as an additional term in Eq. 13.5. A discussion on the affects of frictional forces on shear strength was discussed by Poloski et al. (2006b).

To use this Eq. 13.5 during sedimentation, the gel time for shear strength calculation must be adjusted to maintain a constant shear strength due to the sedimentation process while adjusting to the transient shear strength curve that matches the settled solids concentration. This is done through a numerical simulation constructed by considering two periods of time during the sedimentation process,  $t_0$  and  $t_1$ , where  $t_0 < t_1$ . As sedimentation proceeds, solids concentration increases from an initial value at time  $t_0$ . The transient shear strength curve for the new solids concentration shifts due to the new solids concentration at time  $t_1$ . Therefore, a correction to the gel time is made to keep the shear strength constant due to sedimentation but reflects the new transient shear strength curve at the more fully settled solids concentrations. The correction for this shear strength gel time can be mathematically found as Eq. (13.7). The new gel time is calculated as Eq. (13.8).

$$\Delta t_g = \frac{1}{k} \ln \left[ \frac{(\tau_{O,0}^B - \tau_{\infty,0}) + (\tau_{\infty,0} - \tau_{\infty,1}) e^{-k(t_0 - t_{g,0})}}{(\tau_{O,1}^B - \tau_{\infty,1})} \right] \quad (13.7)$$

$$t_{g,1} = t_{g,0} + \Delta t_g \quad (13.8)$$

From these equations, the rheological properties are observed to grow exponentially with solids concentration. Fully settled slurries typically exhibit large rheological properties, and a level of dilution is required for retrieval and processing. In this section, a 50% by volume dilution from the fully settled configuration is assumed as a realistic tank retrieval condition (the actual amount of diluant used will vary with retrieval technology and engineering parameters). When fully settled, the sludge interface level would then be at 75% of the total vessel height. Several process scales should be considered in this assessment. A summary of several significant height scales are shown in Table 13.1.

**Table 13.1.** Typical Process Heights

Process System	Length Scale	
	SI	Imperial
Piping	0.1 m	3.9 in
Small Vessel	1 m	3.3 ft
Large Vessel	10 m	33 ft

Since the sedimentation experiments typically occurred under ambient temperature conditions, modeling was limited to rheological data in the 20°–35°C temperature range. The average sedimentation parameters from Section 11,  $\alpha$  and  $C$ , for each tank were used in the simulation. Bingham consistency and yield stress modeling parameters from Section 12 were also applied. Table 13.2 shows the values used for each of the variables in these equations. Only limited data were available for this analysis, and the relative volume of each waste type analyzed compared with the total volume of the sludge waste types is shown in Figure 13.1.

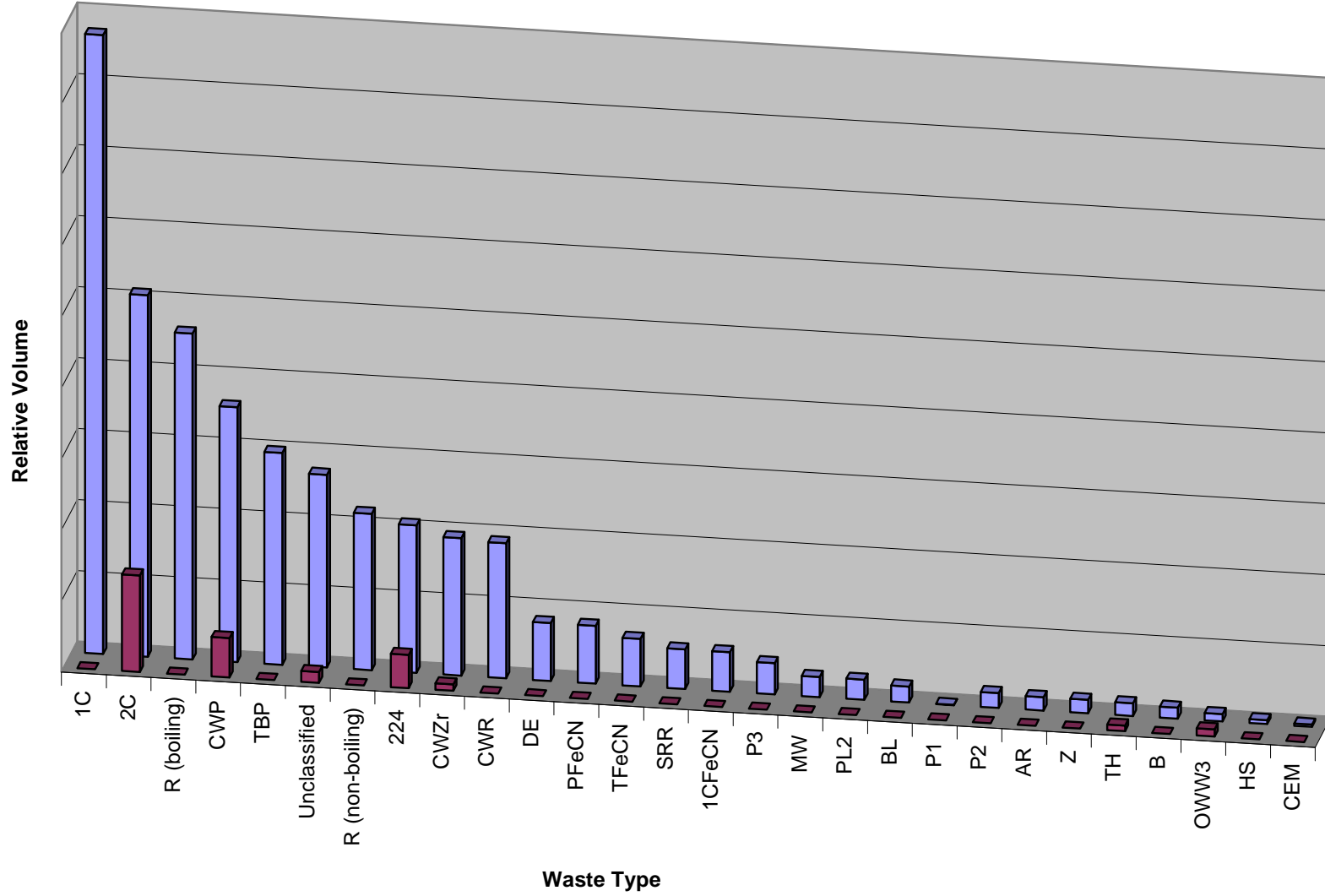
With these values, estimates on the transient growth of rheological parameters as a function of depth were performed. The results at the three length scales are shown in Appendix E. Figures 13.2–13.4 show typical examples of these results. The figures indicate that sedimentation will occur faster in the small-scale systems such as pipes than in the larger systems such as plant vessels, reaching fully settled configurations on the order of tens, hundreds, and thousands of hours for each of the process scales from smallest to largest, respectively.

However, as sedimentation proceeds, the solids concentration at the bottom of the layer is significantly higher than at the top. This result indicates that rheological properties significantly increase from the top of the sediment bed to the bottom. A thick sludge heel begins to form at the bottom of the sediment bed. The sludge heel then reaches the maximum rheological properties due to gravitational forces that increase solids concentration at the bottom of the sediment bed and interparticle bonds that develop as the particles remain quiescent. The thickness of this heel then appears to expand, as these forces are maximized from the bottom of the bed to the top, until the entire sediment bed has the same rheological properties as the heel. Also note that the heel will also contain coarse and dense particles that will slowly settle to the bottom of the sediment layer if the required agitation is not sufficient to suspend the particles during normal operation or if the rheological properties of the sludge are not sufficient to suspend the particles during the sedimentation period. The thick sludge heel may be difficult to retrieve and reaches a substantial portion of the overall sediment bed on the order of 10, 100, and 1000 hours for each process scale considered from smallest to largest. This process is shown graphically in Figure 13.5.

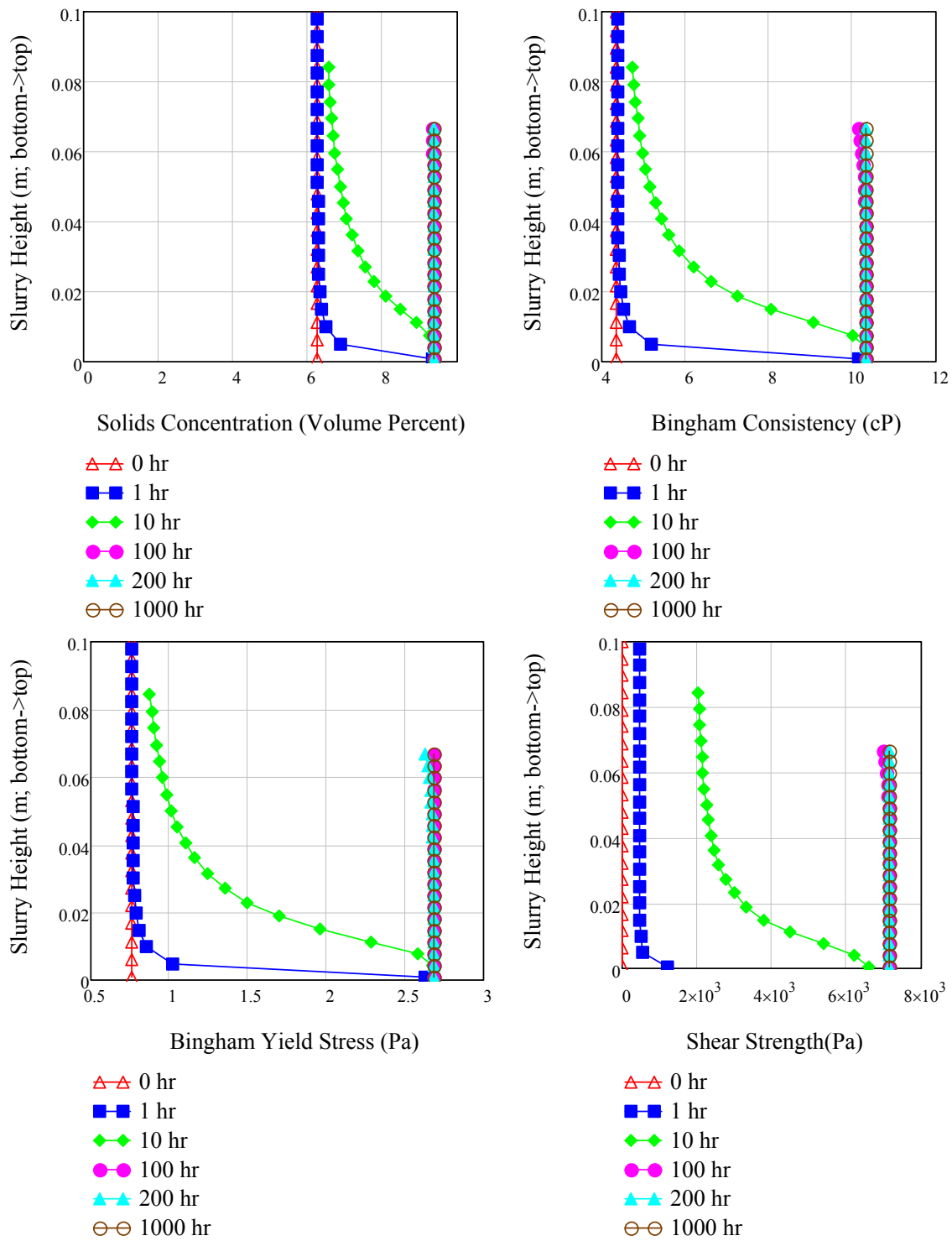
**Table 13.2.** Variable Values used in Transient Modeling

Waste Type	Waste Tank	Waste Status	Temperature Category (°C)	Consistency Parameter, <i>a</i> (cP)	Consistency Parameter, <i>b</i> (-)	Yield Stress Parameter, <i>c</i> (Pa)	Yield Stress Parameter, <i>d</i> (-)	Maximum Measure Shear Strength (Pa)	Shear Strength Parameter, <i>c<sub>∞</sub></i> , (Pa)	<i>C</i> (mm/hr)	<i>α</i> (mm/hr)
Source →			Table 12.1				Figure 11.3	Eq. (13.6)	Table 10.1		
224	B-202	Washed	20-35	1.51	36	7.21E+04	2.94	750	5.25E+07	16.9	0.38
224	B-203	Washed	20-35	1.30	72	1.31E+07	3.80	2,280	4.03E+10	21.8	0.27
224	T-203	Washed	20-35	1.08	79	2.50E+05	2.60	3,770	5.79E+08	16.8	0.17
2C	T-110	Washed	20-35	1.16	46	1.21E+04	2.68	70	2.39E+06	11.3	0.23
CWP	C-104	Salt Cake	20-35	1.25	12	2.79E+02	2.40	7,077	2.12E+06	4.3	0.40
CWP	C-104	Washed	20-35	0.78	28	4.13E+03	3.11	7,077	1.14E+07	4.3	0.40

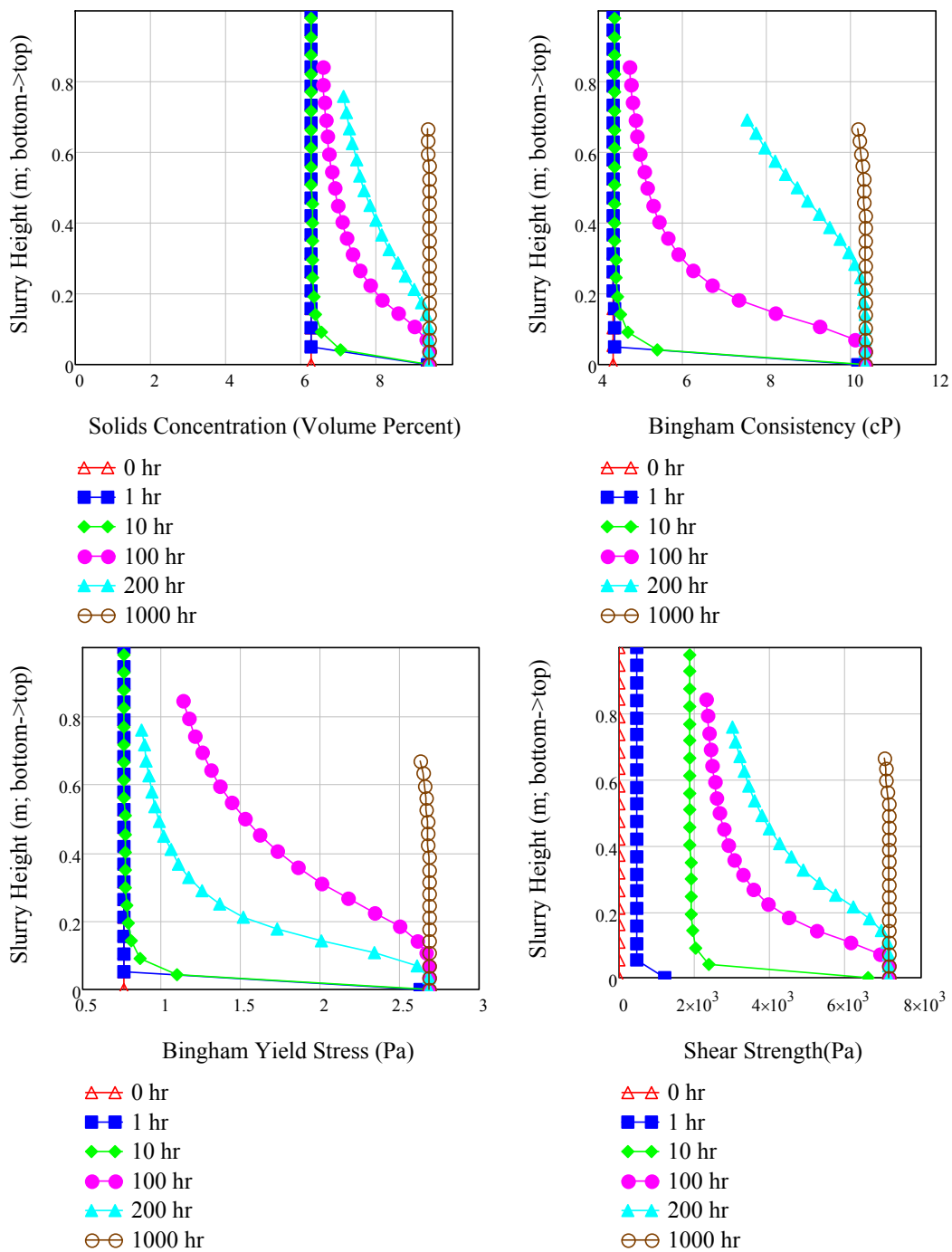




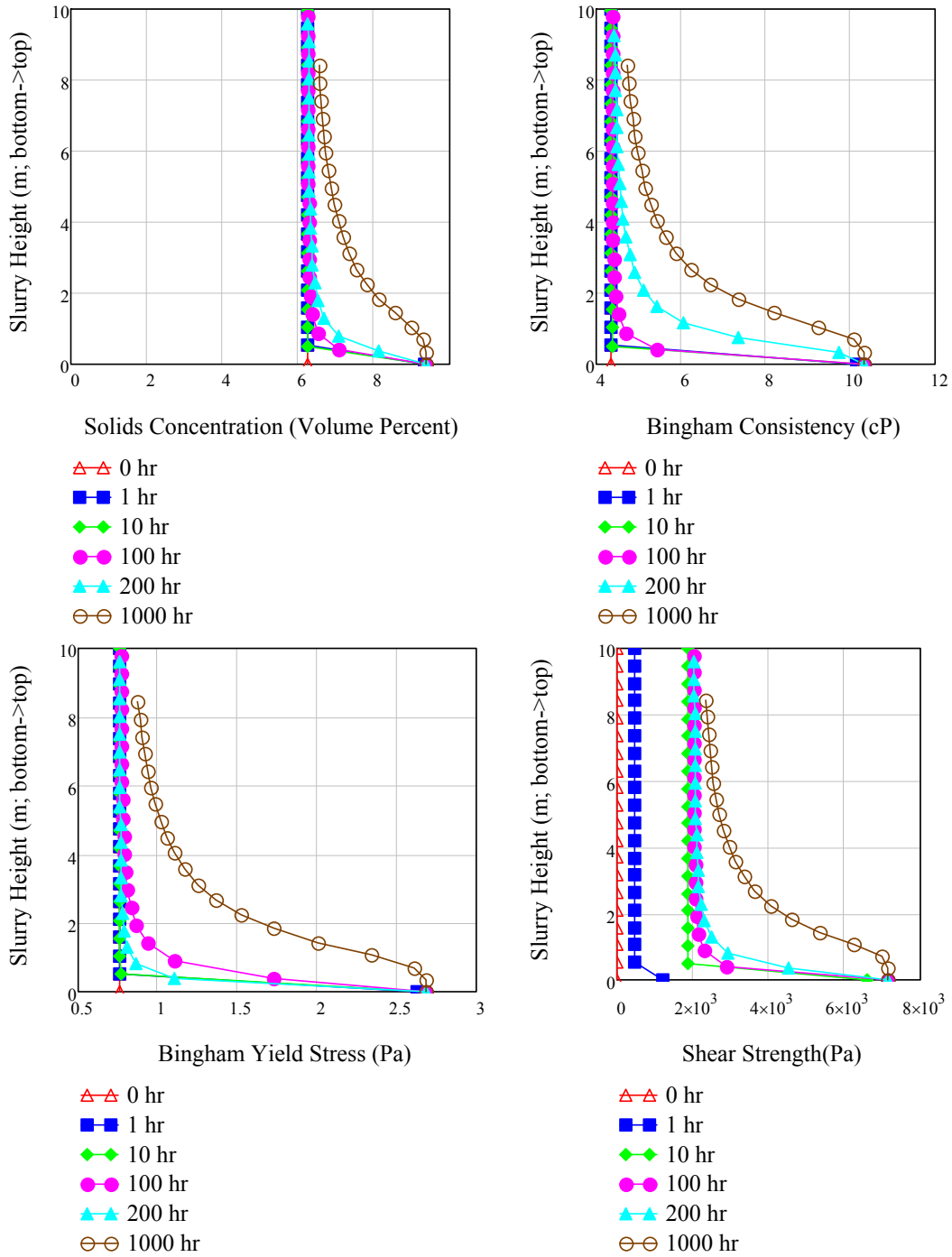
**Figure 13.1.** Relative Volume of Waste Types Analyzed based on Waste Tank Data Available for Transient Modeling



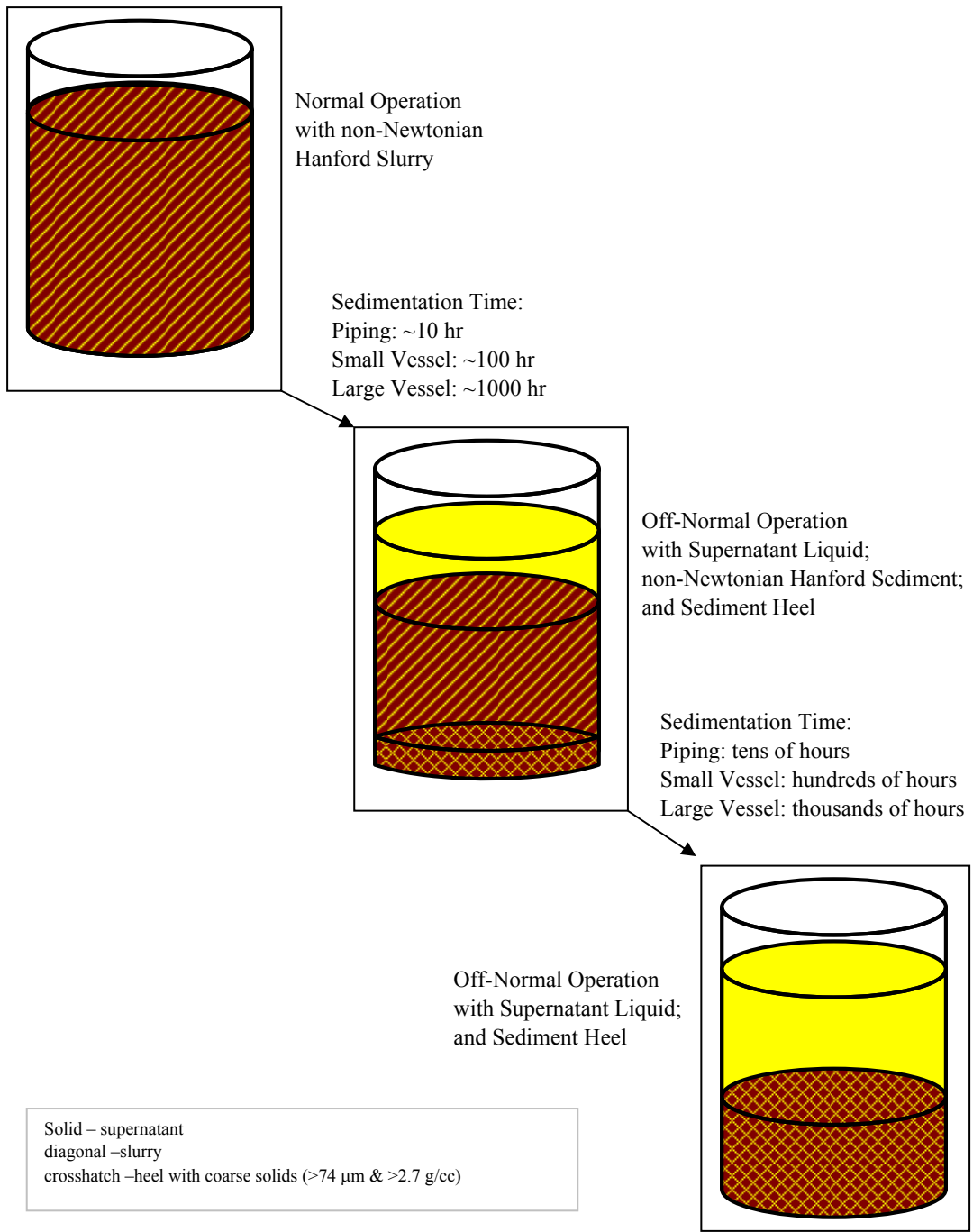
**Figure 13.2.** Predicted Sludge Properties from Hanford Tank C-104 with Water Dilution at a Starting Slurry Height of 0.1 m with 33% Volume Excess Supernatant from Fully Settled Configuration; Rheological Properties Taken at a Temperature Range of 20°-35°C.



**Figure 13.3.** Predicted Sludge Properties from Hanford Tank C-104 with Water Dilution at Starting Slurry Height of 1 M with 33% Volume Excess Supernatant from Fully Settled Configuration; Rheological Properties Taken at a Temperature Range of 20°–35°C

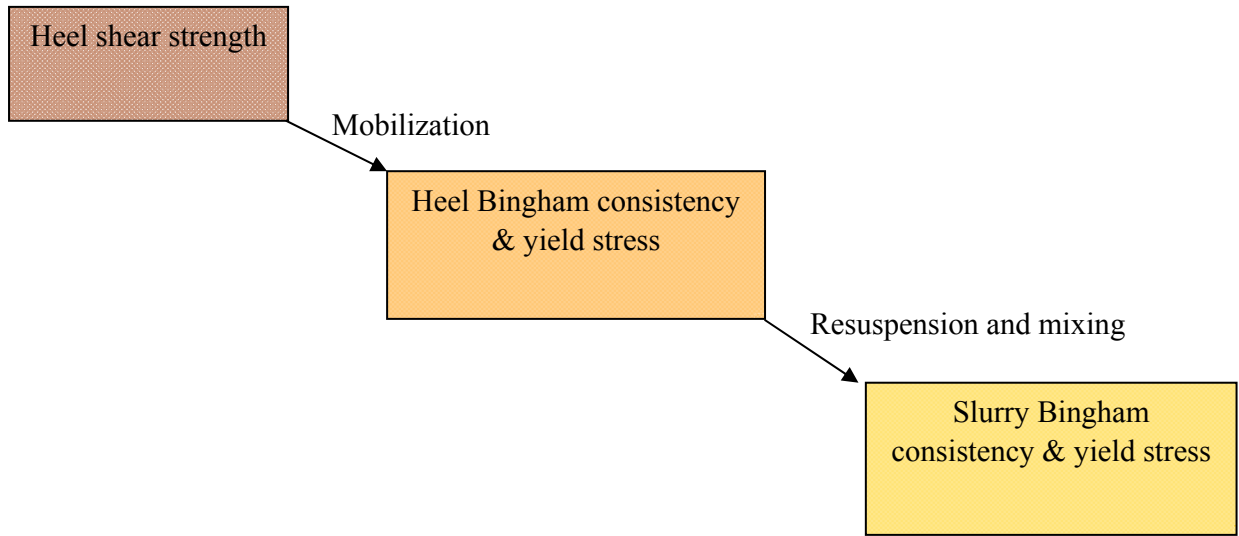


**Figure 13.4.** Predicted Sludge Properties from Hanford Tank C-104 with Water Dilution at Starting Slurry Height of 10 M with 33% Volume Excess Supernatant from Fully Settled Configuration; Rheological Properties Taken at a Temperature Range of 20°-35°C



**Figure 13.5.** Illustration of Development of Sludge Process Heel and Fully Settled Configuration at Various Process Scales

Recovery from these slurry configurations will require the application of all of the parameters identified in this table. Initially the sediment will be gelled to some extent, due to the development of interparticle bonds as the particles remain quiescent and in close proximity, and will possess a shear strength threshold that must be overcome. After the sediment is mobilized, the Bingham consistency and yield stress parameters will be elevated due to the large concentration of undissolved solids in the sediment bed. As mixing proceeds and supernatant liquid is blended into the sediment, the rheological properties will drop to the normal operation range when the slurry is fully suspended. This is shown graphically in Figure 13.6.



**Figure 13.6.** Rheological Properties Encountered During Recovery from Process Upset Conditions

## 14.0 Rheology Summary and Processing Scenarios

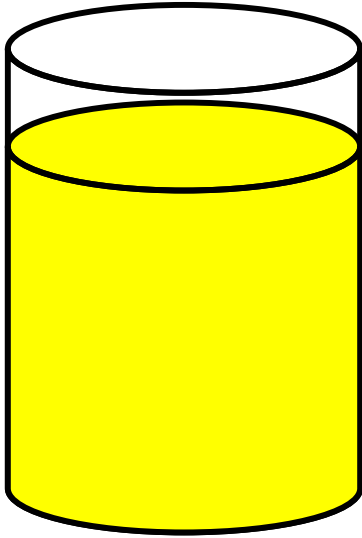
The data discussed in this report can be applied to a wide variety of process conditions. Three major process systems where these data apply are as flow in process vessels, vertical piping, and horizontal piping. In these process systems, several sludge configurations can be identified as potential operational scenarios. These scenarios and sludge configurations are shown in Figures 14.1 through 14.3 for process vessels (e.g. WTP EFRT issue M3), vertical piping, and horizontal piping (e.g. WTP EFRT issue M1), respectively.

Table 14.1 provides a summary of the rheological parameters for each of the fluid layers shown in the associated process scenario figures. This table was compiled from the previous sections on sedimentation, shear strength, Bingham rheological parameters, and supernatant viscosity. In addition, the section discussing transient rheological modeling was summarized to provide an indication of the time scales for rheology regrowth at various process length scales. Recovery from these slurry configurations will require the application of all of the parameters identified in Table 14.1 through the process illustrated in Figure 13.6.

**Table 14.1.** Range of Rheological Parameters and Regrowth Times at Typical Process Scales

Category	Heel Shear strength	Slurry/Sediment Heel Bingham Yield Stress	Slurry/Sediment Heel Bingham Consistency	Supernatant Viscosity
Min <sup>(a)</sup>	40 Pa	0 Pa	1 cP	1 cP
Median <sup>(a)</sup>	700 Pa	1.5 Pa	8 cP	8 cP
Max <sup>(a)</sup>	25,000 Pa	40 Pa	110 cP	30 cP
Tank heel property after 10 hours of sedimentation in process piping (0.1 m sludge height)	25,000 Pa	40 Pa	110 cP	n/a
Tank heel property after 100 hours of sedimentation in a medium-scale vessel (1 m sludge height)	25,000 Pa	40 Pa	110 cP	n/a
Tank heel property after 1000 hours of sedimentation in a large-scale vessel (10 m sludge height)	25,000 Pa	40 Pa	110 cP	n/a
(a) Statistics performed on all compiled data discussed in this report. n/a – not applicable.				

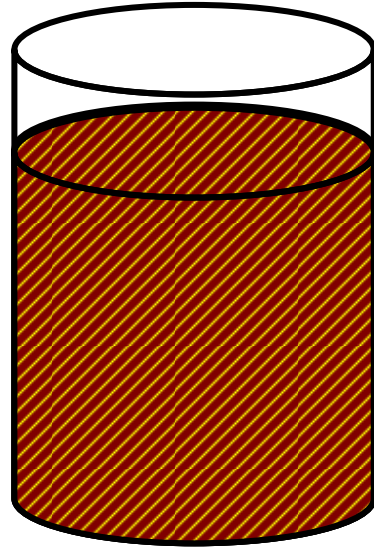
Normal operation with Newtonian fluid



Process impacts:

- cloud height
- blend times

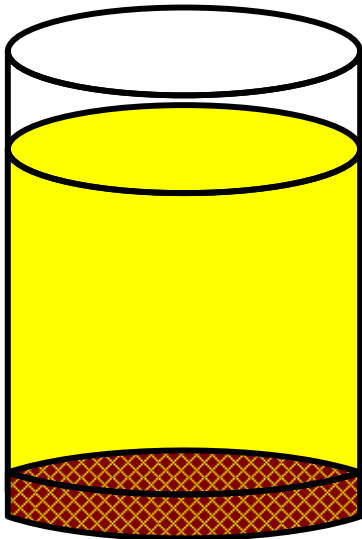
Normal operation with non-Newtonian fluid



Process impacts:

- mixing performance
- gas retention & release

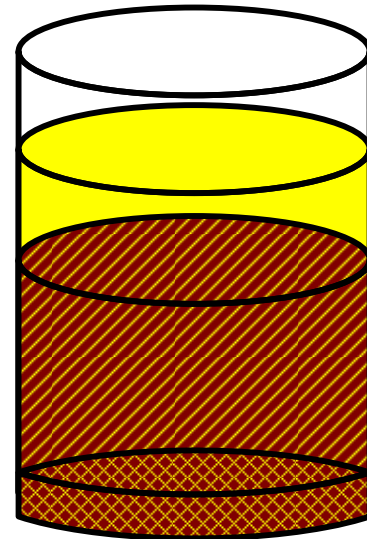
Off-normal operation with Newtonian fluid



Process impacts:

- off-bottom resuspension of solids
- blend time of solids layer

Off-Normal operation with non-Newtonian fluid



Process impacts:

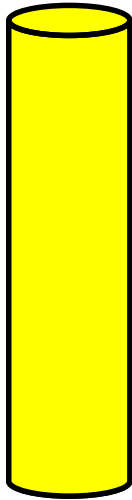
- restart of mechanical agitators/PJMs
- off-bottom resuspension of solids
- blend time liquid/solids layer
- gas retention & release

Solid – supernatant; diagonal – slurry; crosshatch – heel with coarse solids (>74  $\mu\text{m}$  & >2.7 g/cc)

**Figure 14.1.** Example Operational Scenarios for Process Vessels



Normal operation with Newtonian fluid



Process impacts:

- critical flow velocity

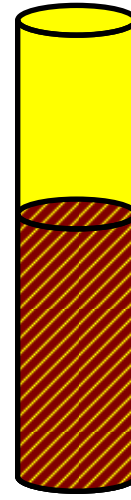
Normal operation with non-Newtonian fluid



Process impacts:

- flow velocity and pressure drop
- flow regime

Off-normal operation with non-Newtonian fluid



Process impacts:

- restart
- flushing effectiveness

Solid – supernatant; diagonal – slurry; crosshatch – heel with coarse solids (>74 μm & >2.7 g/cc)

**Figure 14.2.** Example Operational Scenarios for Vertical Process Piping

Normal operation with Newtonian fluid



Process impacts:

- critical flow velocity

Normal operation with non-Newtonian fluid



Process impacts:

- flow velocity and pressure drop
- flow regime

Off-normal operation with Newtonian fluid



Process impacts:

- restart
- flushing effectiveness

Off-Normal operation with non-Newtonian fluid



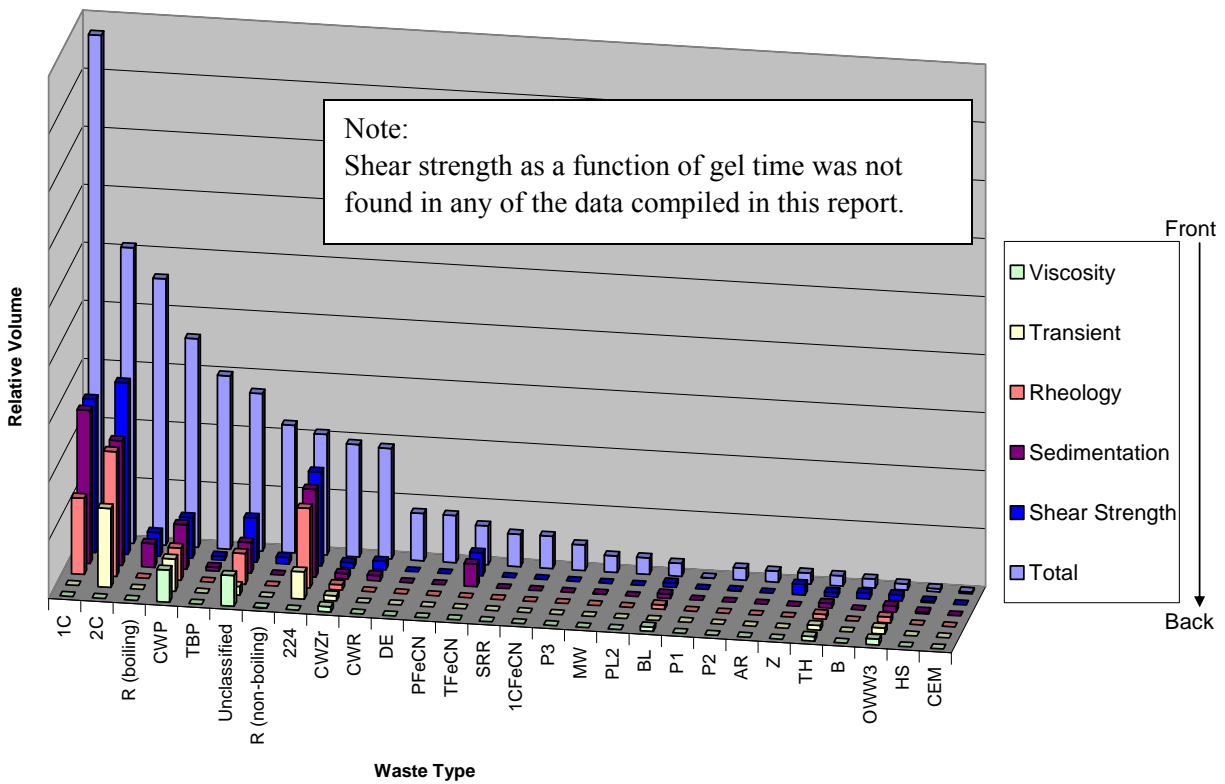
Process impacts:

- restart
- flushing effectiveness

Solid – supernatant; diagonal – slurry; crosshatch – heel with coarse solids (>74 μm & >2.7 g/cc)

**Figure 14.3.** Example Operational Scenarios for Horizontal Process Piping

Rheology data and associated physical properties for Hanford tank wastes were compiled from all the readily available reports, but many gaps were observed when analyzing the data. These data include in situ as well as laboratory analysis of samples removed from the tanks. The gaps in the waste types analyzed are reported in each section of the report. Figure 14.4 provides a summary of these gaps. The relative volume of wastes modeled for liquid viscosity, sedimentation, shear strength, rheological parameters (Bingham plastic model), and rheological parameters as a function of settling are plotted as a function of waste type.



**Figure 14.4.** Relative Volume of Waste Types Modeled Based on Waste Tank Data Available for Liquid Viscosity, Sedimentation, Shear Strength, Rheology, and Transient Modeling Compared to the Total Volume of Each Sludge Waste Type

## 15.0 References

Bechtel National, Inc. July 2004. *WTP Integrated Processing Strategy Description*. 24590-WTP-3YD-50-00002 Rev 0, BNI, Richland, Washington.

Bechtel National, Inc. 2006. *Issue Response Plan for Implementation of External Flowsheet Review Team (EFRT) Recommendations - M3, Inadequate Mixing System Design*. 24590-WTP-PL-ENG-06-0013, Rev 000, Bechtel National, Inc., Richland, Washington.

Bechtel National, Inc. December 2006. *Integrated Sampling and Analysis Requirements Document*. 24590-WTP-PL-PR-04-0001 Rev 1, BNI, Richland, Washington.

CRC. 1975. *CRC Handbook of Chemistry and Physics, 56<sup>th</sup> Ed.* RC Weast (Ed). CRC Press, Cleveland, Ohio.

Ferraris F and N Martys. 2001. "Fresh Concrete Rheology – Recent Developments." *Materials Science of Concrete VI*, S Mindess and J Skalny, eds., pp. 215-241.

Gauglitz PA and JT Aikin. 1997. *Waste Behavior During Horizontal Extrusion: Effect of Waste Strength for Bentonite and Kaolin/Ludox Simulants and Strength Estimates for Wastes from Hanford Tanks 241-SY-103, AW-101, AN-103, and S-102*. PNNL-11706, Pacific Northwest National Laboratory, Richland, Washington.

Higley BA and DE Place. February 2004. *Hanford Defined Waste Model*, Rev. 5.0. RPP-19822, CH2M Hill Hanford Group, Richland, Washington.

Meacham JE. 2003. *Aluminum Wash and Leach Factors*. RPP-11079, CH2M HILL Hanford Group, Inc., Richland, Washington.

Morrey EV and JM Tingey. 1996. *Comparison of Simulants to Actual Neutralized Current Acid Waste: Process and Product Testing of Three NCAW Core Samples from Tanks 101-AZ and 102-AZ*. PNNL-11098, Pacific Northwest National Laboratory, Richland, Washington.

Poloski AP, PA Meyer, LK Jagoda, and PR Hrma. 2003a. *Technical Basis for LAW Vitrification Stream Physical and Rheological Property Bounding Conditions*. WTP-RPT-098 Rev. 0, Battelle – Pacific Northwest Division, Richland, Washington.

Poloski AP, PR Breidt, JW Chenault, and RG Swoboda. 2003b. *Rheological and Physical Properties of AZ-101 HLW Pretreated Sludge and Melter Feed*. WTP-RPT-096 Rev. 0, Battelle – Pacific Northwest Division, Richland, Washington.

Poloski AP, PA Meyer, LK Jagoda, and PR Hrma. 2004. *Non-Newtonian Slurry Simulant Development and Selection for Pulse Jet Mixer Testing*. PNWD-3495 (WTP-RPT-111 Rev. 0), Battelle – Pacific Northwest Division, Richland, Washington.

Poloski AP, ST Arm, OP Bredt, TB Calloway, Y Onishi, RA Peterson, GL Smith, and HD Smith. 2006a. *Final Report: Technical Basis for HLW Vitrification Stream Physical and Rheological Property Bounding Conditions*. PNWD-3675 (WTP-RPT-112 Rev. 0), Battelle – Pacific Northwest Division, Richland, Washington.

Poloski AP, PR Bredt, RC Daniel, and AE Saez. 2006b. "The Contribution of Frictional Contacts to the Shear Strength of Coarse Glass Bead Powders and Slurries." *Rheologica Acta* 46(2):249-259.

Rassat SD, LA Mahoney, BE Wells, DP Mendoza, DD Caldwell. 2003. *Assessment of Physical Properties of Transuranic Waste in Hanford Single-Shell Tanks*. PNNL-14221, Pacific Northwest National Laboratory, Richland, Washington.

Renko EK. 1996. "A model for batch settling curve." *Water SA*. 22(4)339-344.

Renko EK. 1998. "Modeling hindered batch settling Part II: A model for computing solids profile of calcium carbonate slurry." *Water SA*, 24(4)331-336.

Shephard CL, JB Colson, KO Pasamehmetoglu, C Unal, JN Edwards, and J Abbott. 1994. *Theory of Operation for the Ball Rheometer*. PNL-10240, Pacific Northwest National Laboratory, Richland, Washington.

Speers RA, KR Holme, MA Tung, and WT Williamson. 1987. "Drilling fluid shear stress overshoot behavior." *Rheologica. Acta*, 26:447-452

Stewart CW, JM Alzheimer, ME Brewster, G Chen, RE Mendoza, HC Reid, CL Shephard, and G Terrones. 1996. *In Situ Rheology and Gas Volume in Hanford Double-Shell Waste Tanks*. PNNL-11296, Pacific Northwest National Laboratory, Richland, Washington.

Wells BE, MA Knight, EC Buck, RC Daniel, SK Cooley, LA Mahoney, PA Meyer, AP Poloski, JM Tingey, WS Callaway, III, GA Cooke, ME Johnson, MG Thien, DJ Washenfelder, JJ Davis, MN Hall, G Smith, SL Thomson, and Y Onishi. 2007. *Estimate of Hanford Waste Insoluble Solid Particle Size and Density Distribution*. PNWD-3824 (WTP-RPT-153 Rev. 0) Battelle – Pacific Northwest Division, Richland, Washington.

Zhou Z, PJ Scales, and DV Boger. 2001. "Chemical and physical control of the rheology of concentrated metal oxide suspensions." *Chemical Engineering Science*, 56: 2901-2920.

## **Appendix A**

### **Tabulation of Available Rheology Data and Associated Physical and Chemical Data for Hanford Tank Wastes**

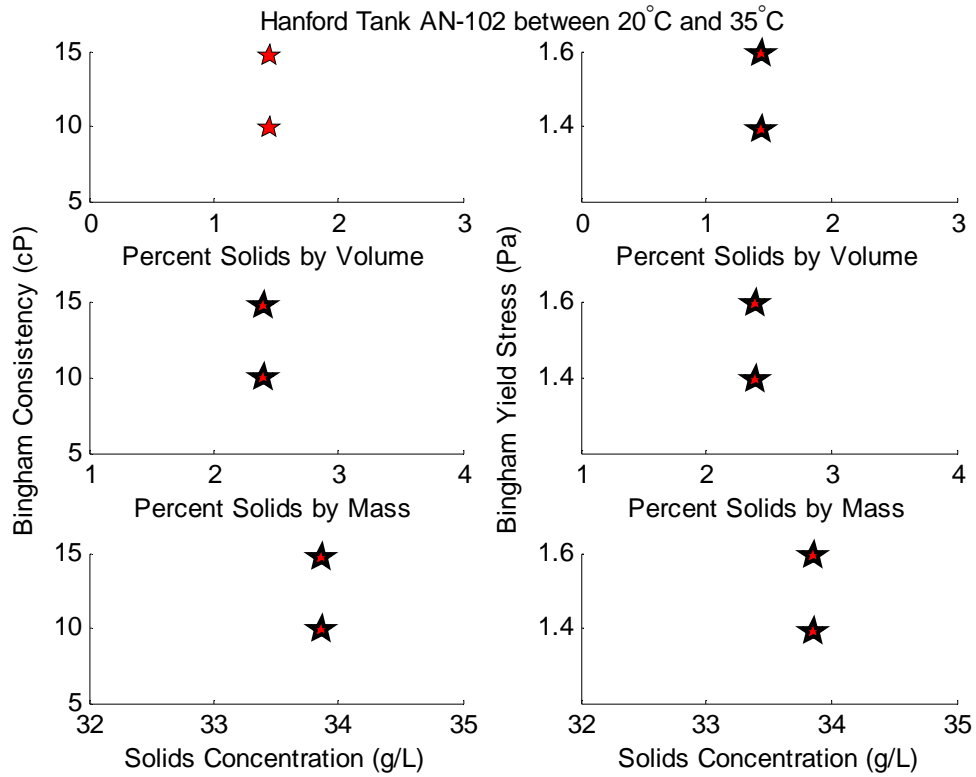
**Appendix A – Tabulation of Available Rheology Data  
and Associated Physical and Chemical Data  
for Hanford Tank Wastes**

## **Appendix B**

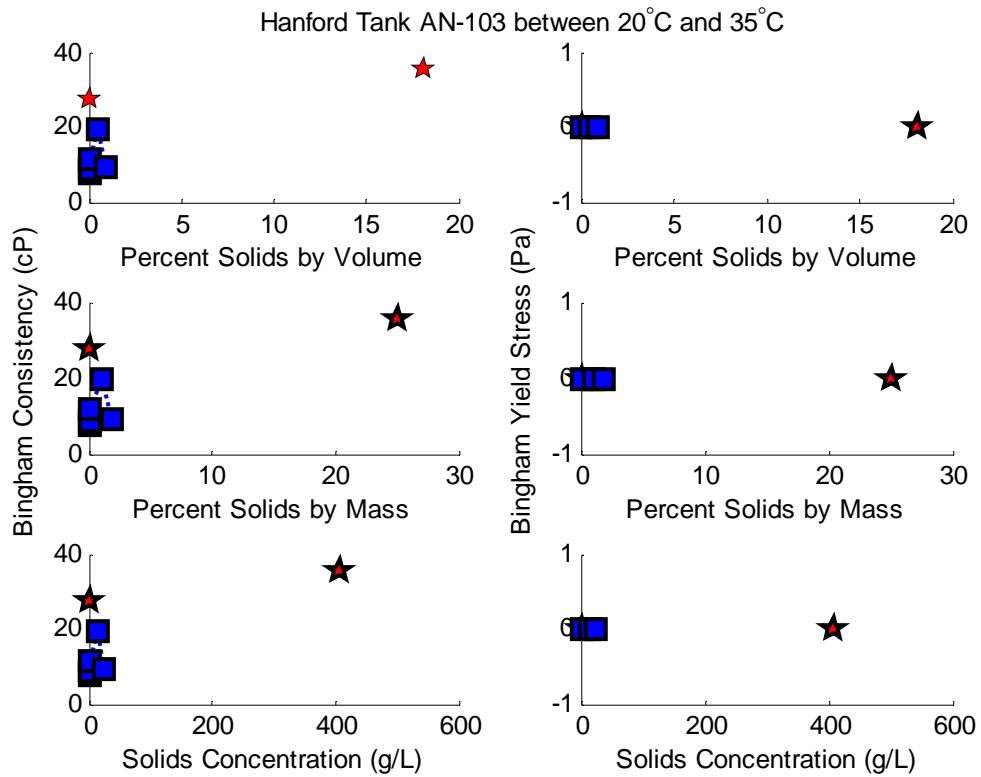
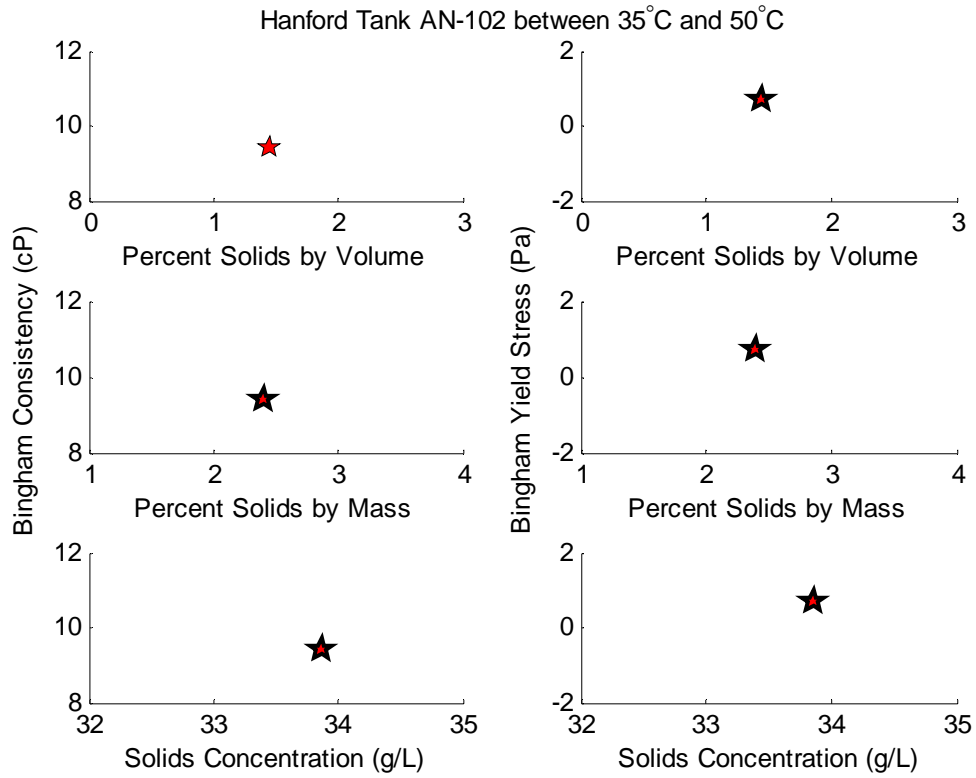
### **Raw Data Used in Evaluating Correlations of the Bingham Plastic Model Parameters with Solids Content**

# Appendix B – Raw Data Used in Evaluating Correlations of the Bingham Plastic Model Parameters with Solids Content

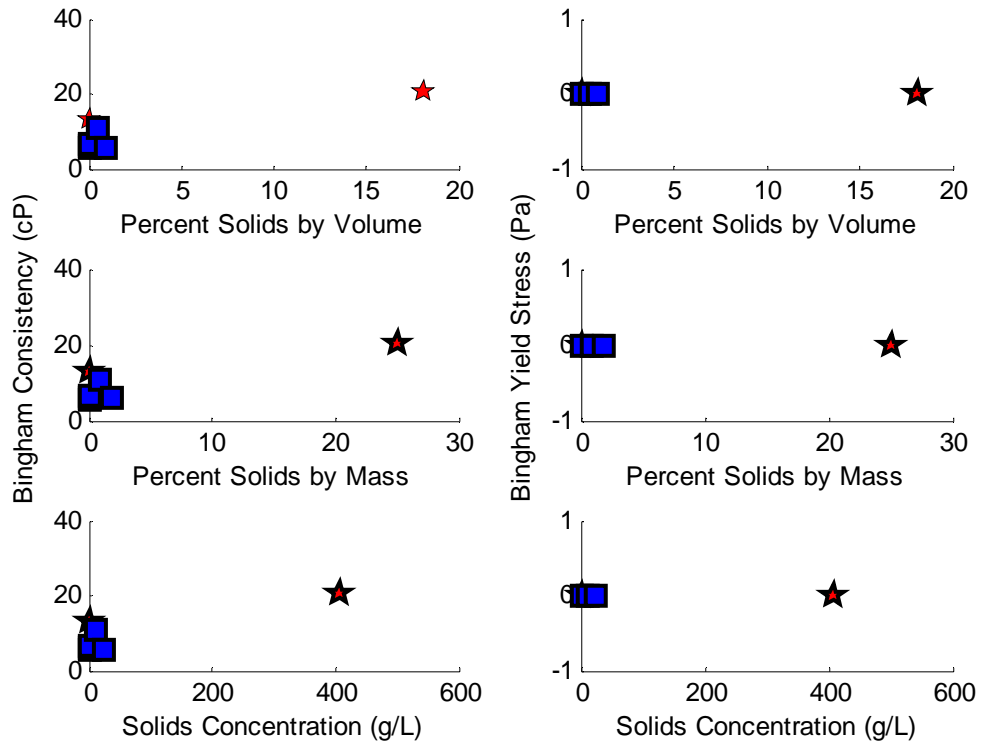
In the figures in this appendix, the stars = as-received tank waste; squares = water added as diluent; and circles = post washing and caustic leaching.



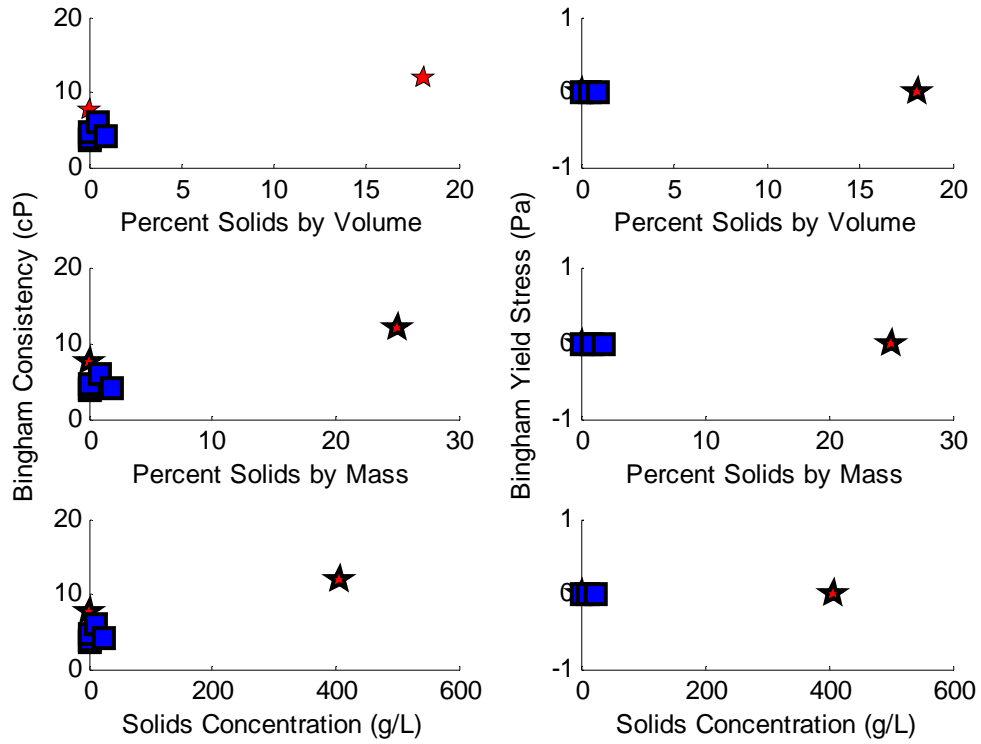




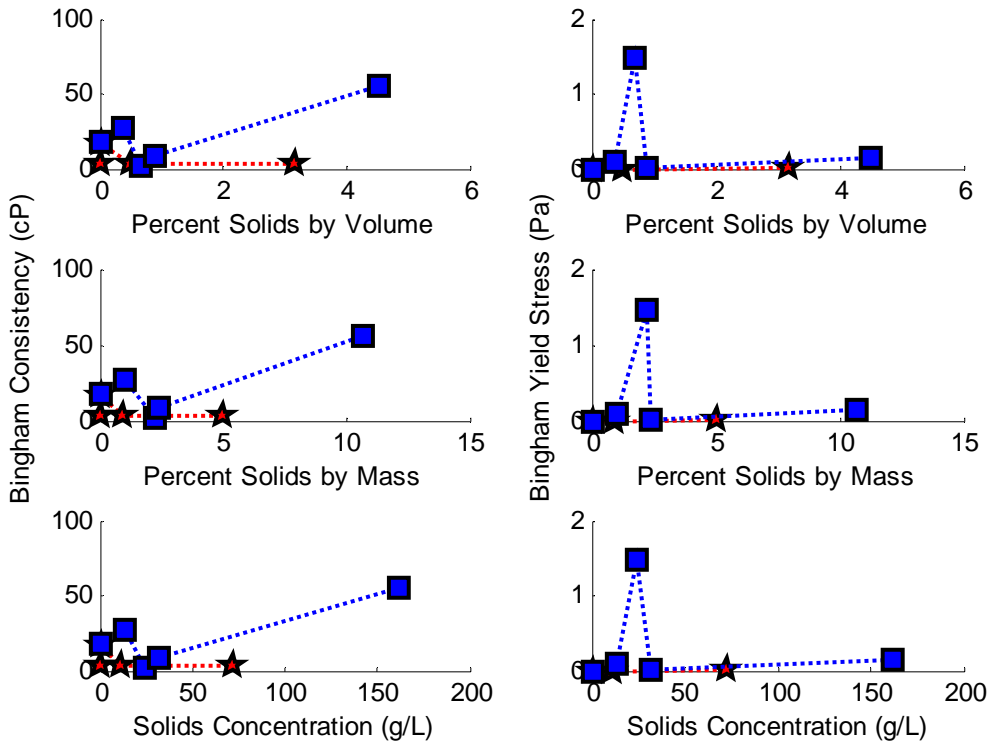
Hanford Tank AN-103 between 35°C and 50°C



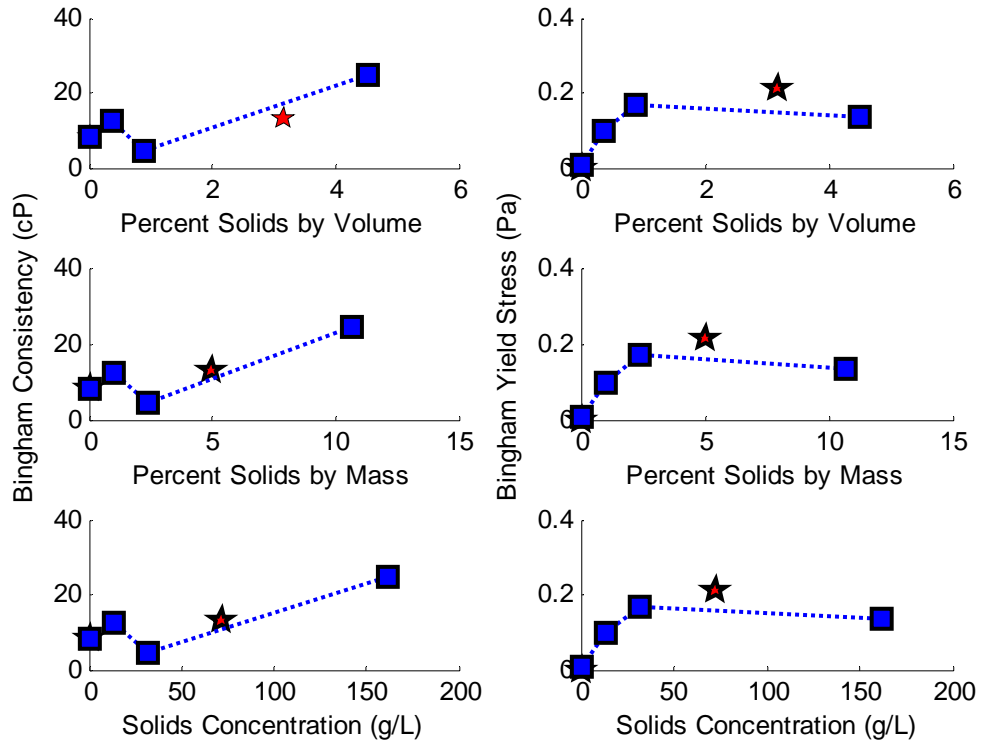
Hanford Tank AN-103 between 50°C and 65°C

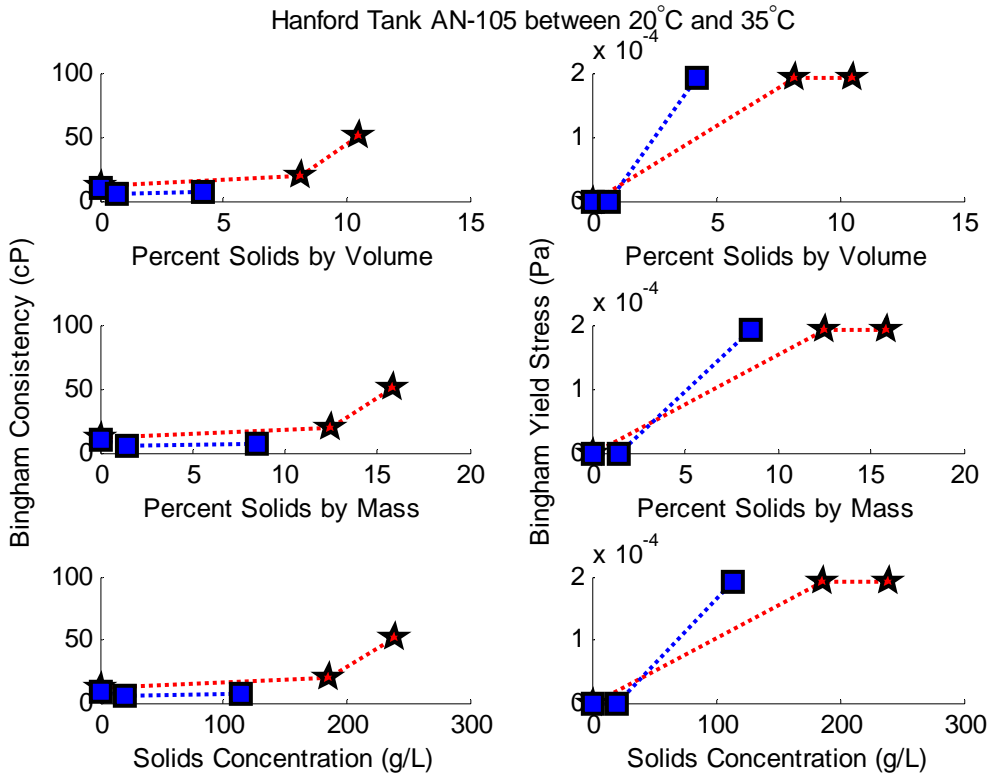
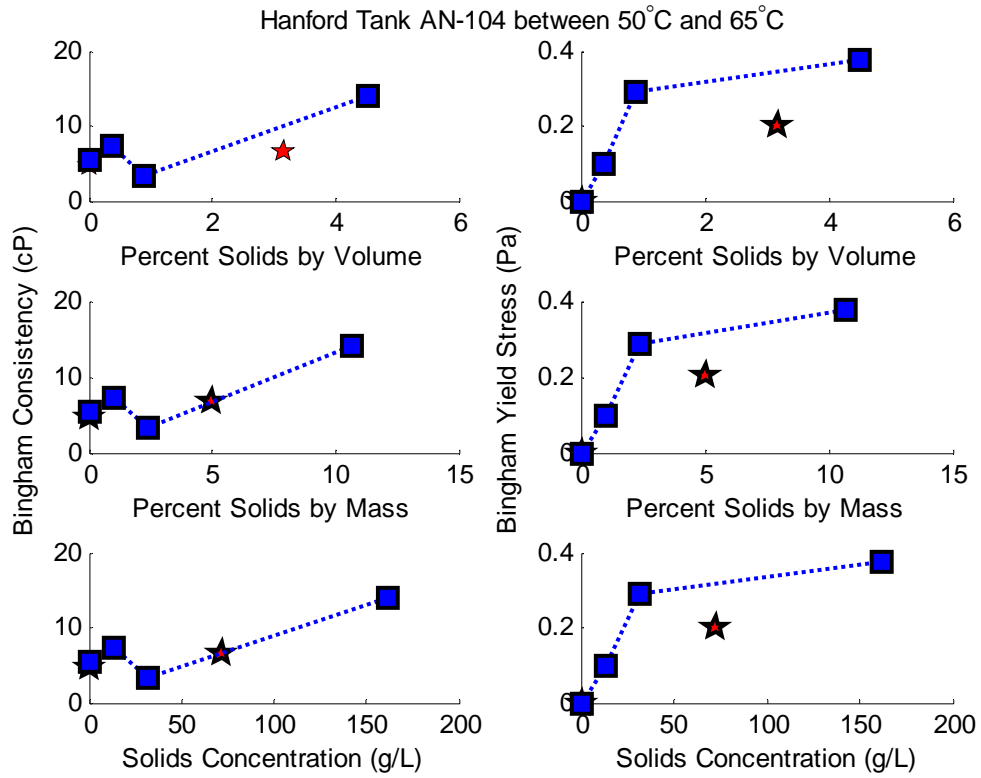


Hanford Tank AN-104 between 20°C and 35°C

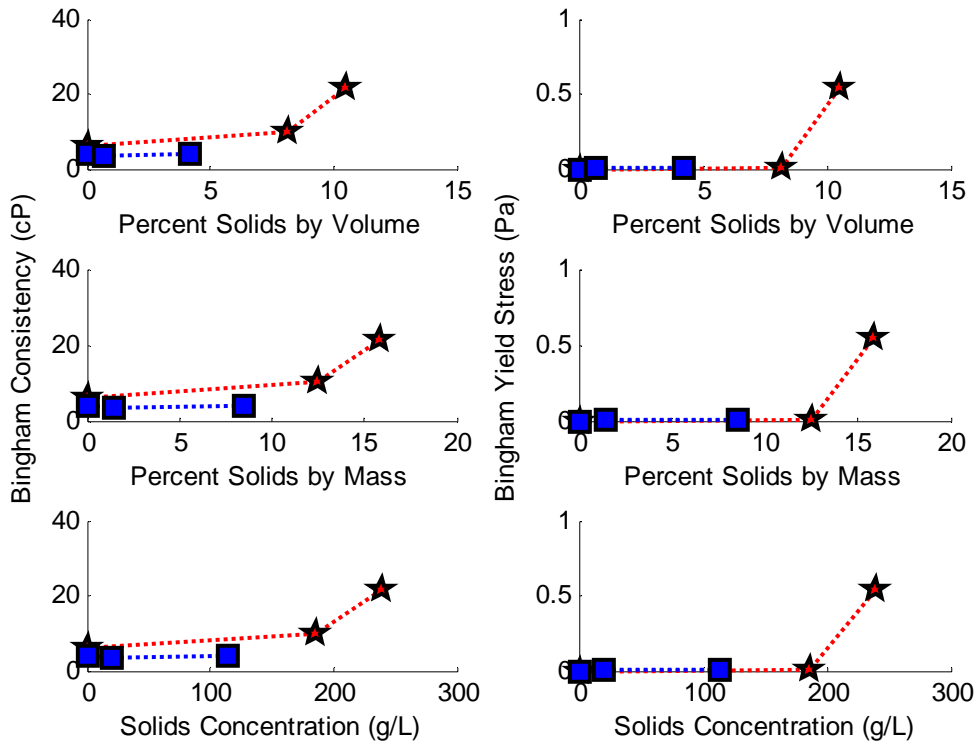


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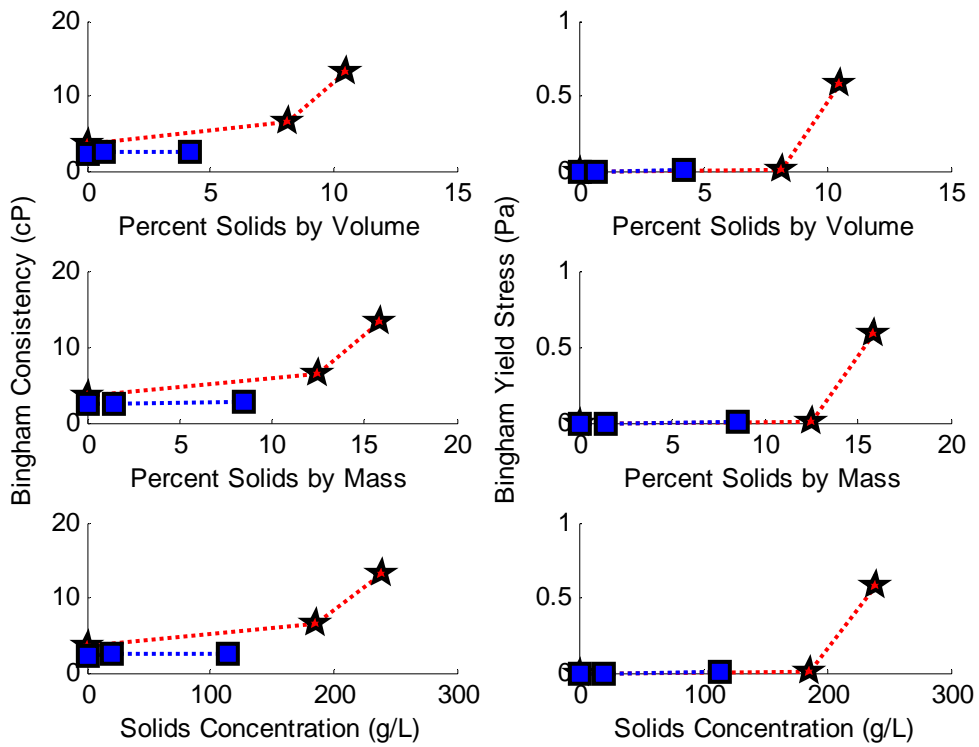


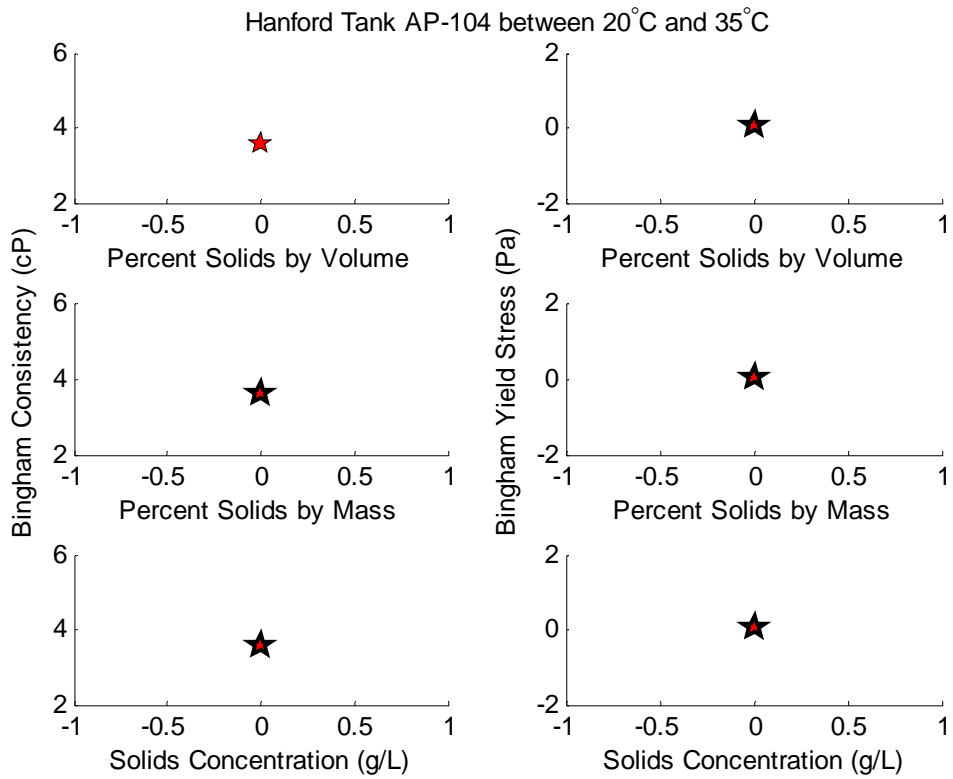
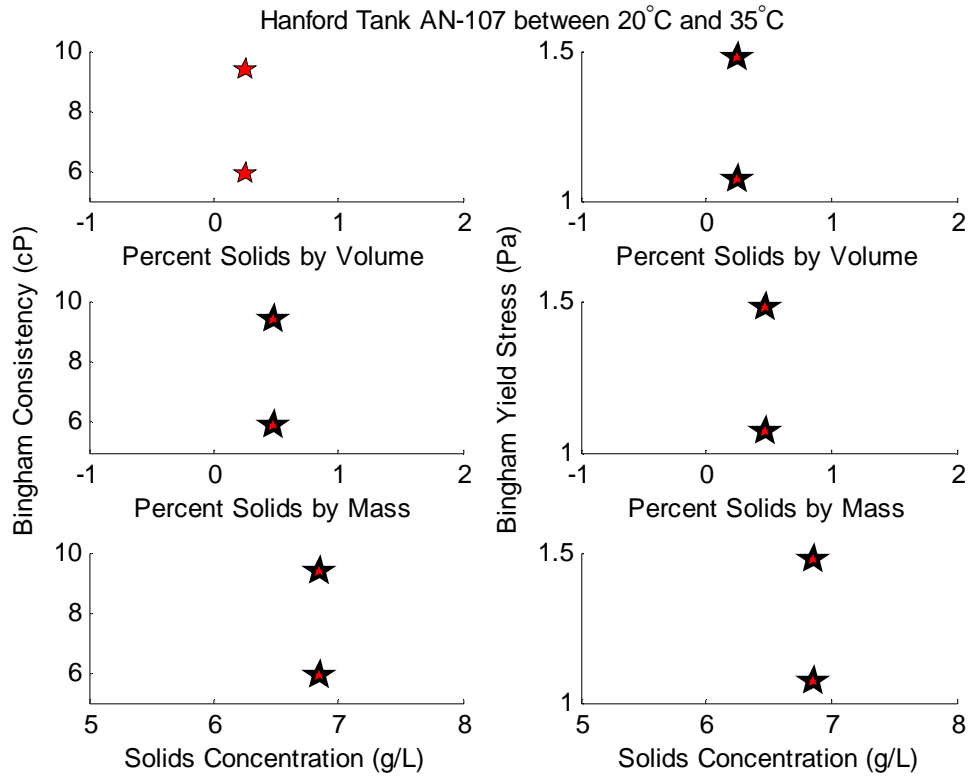


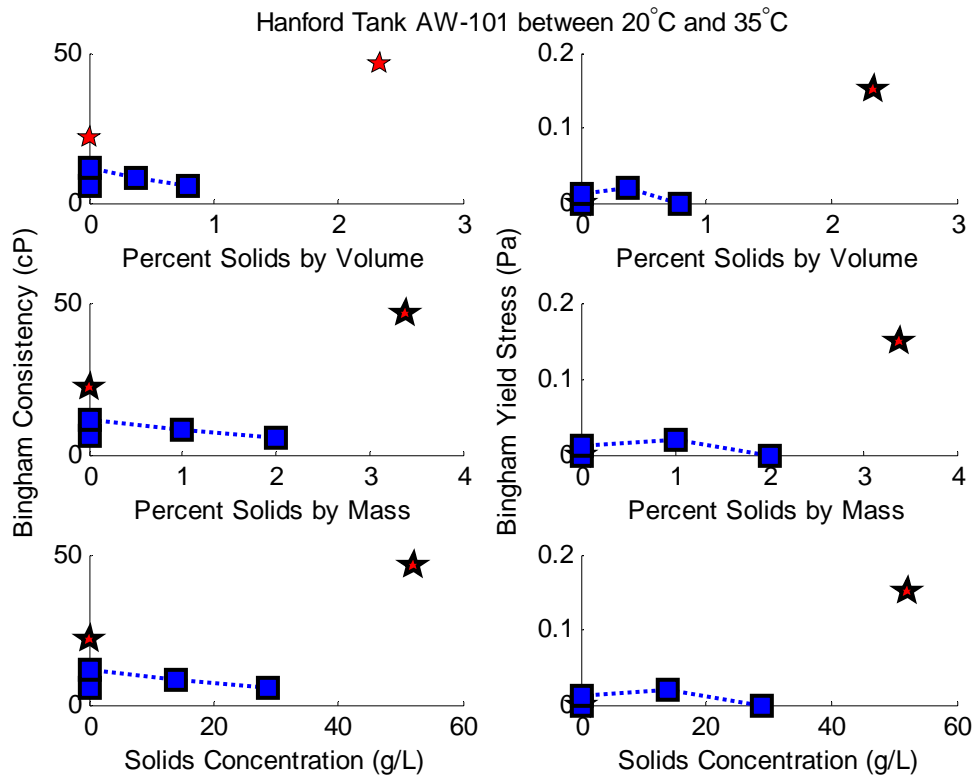
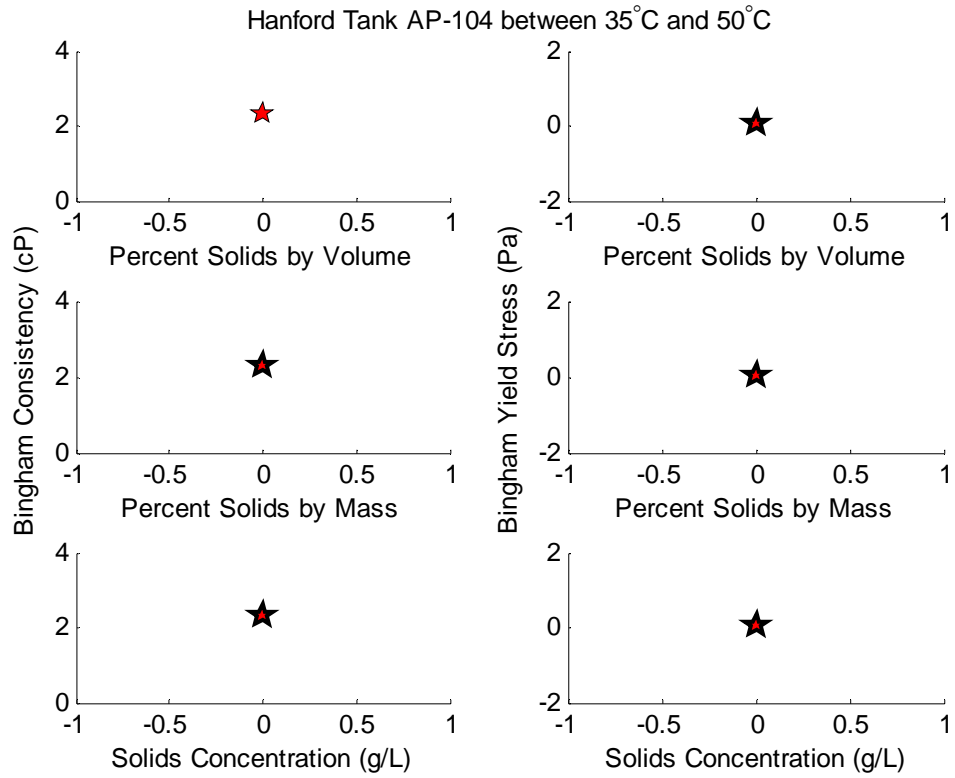
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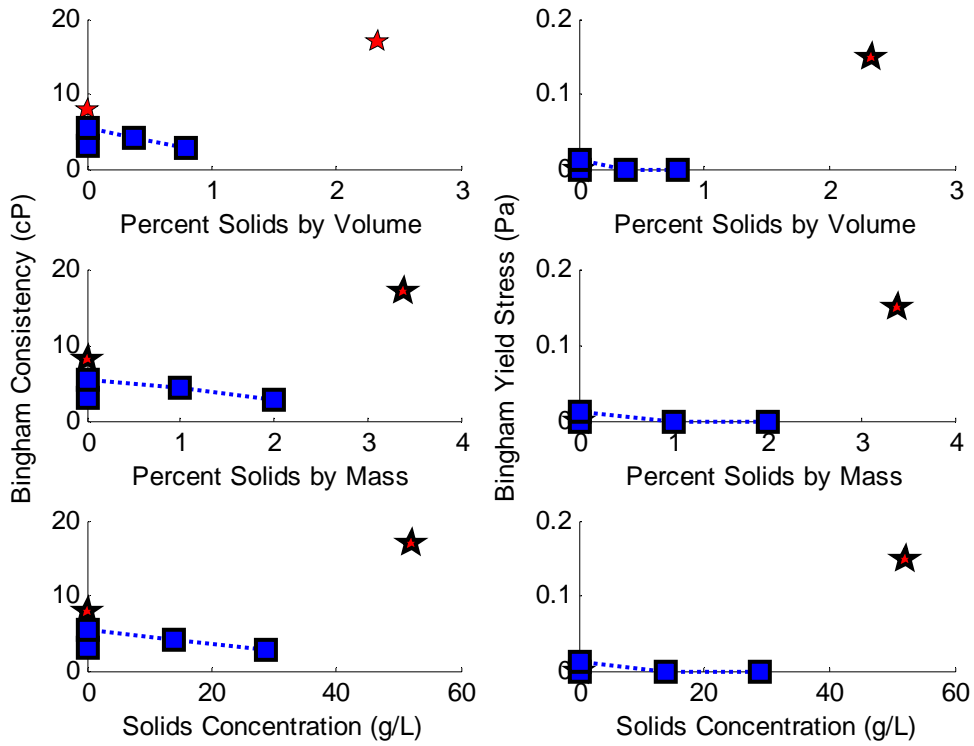
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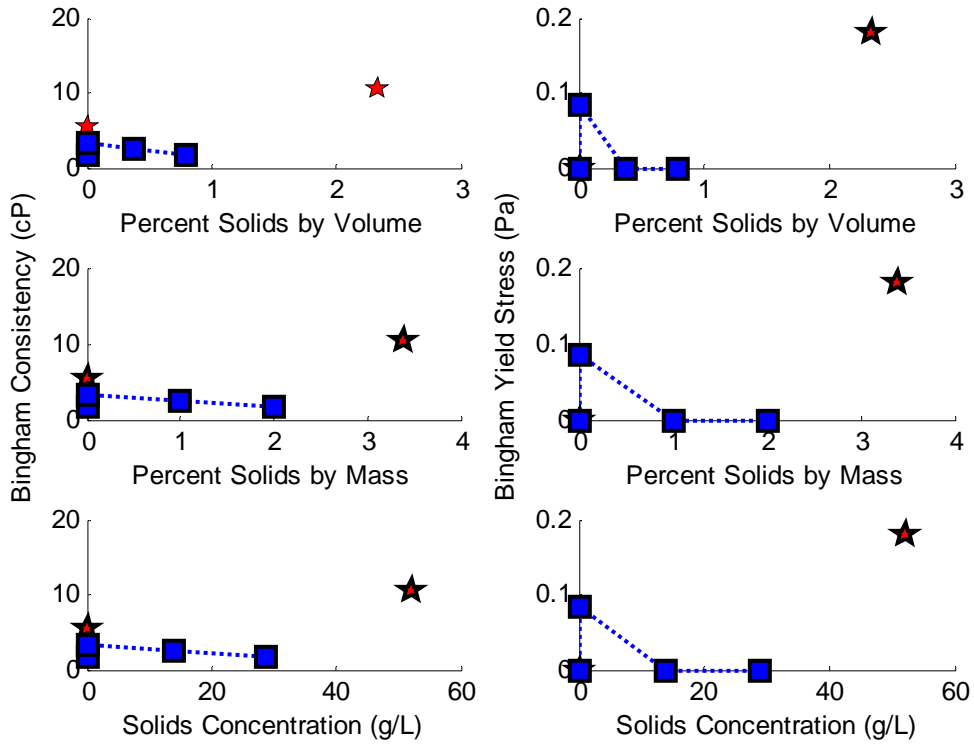




Hanford Tank AW-101 between 35°C and 50°C

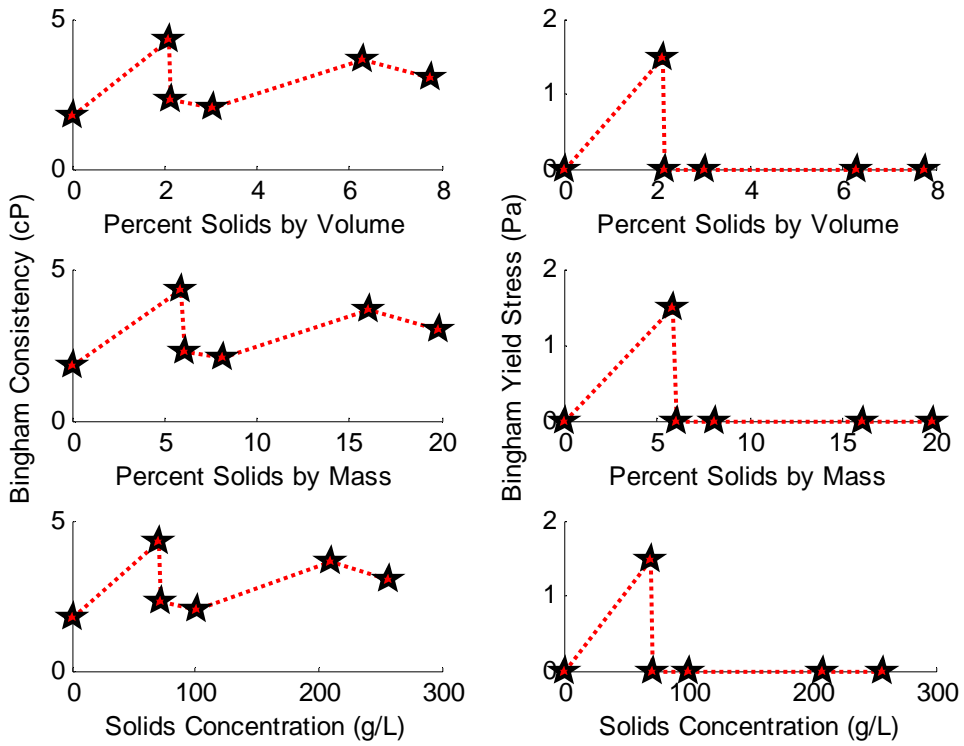


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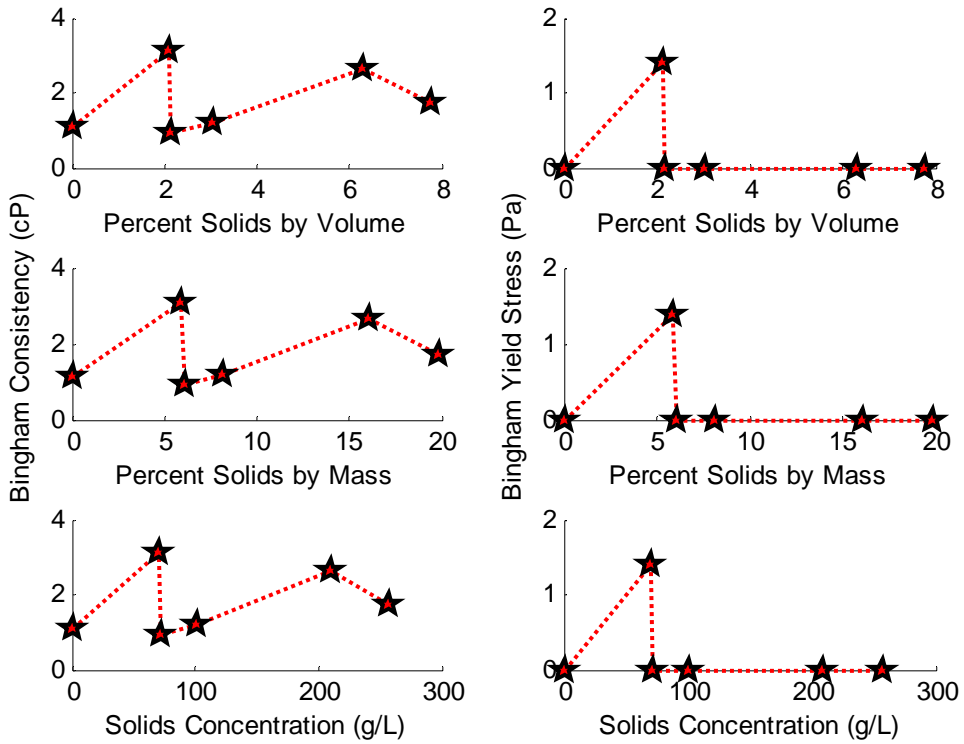




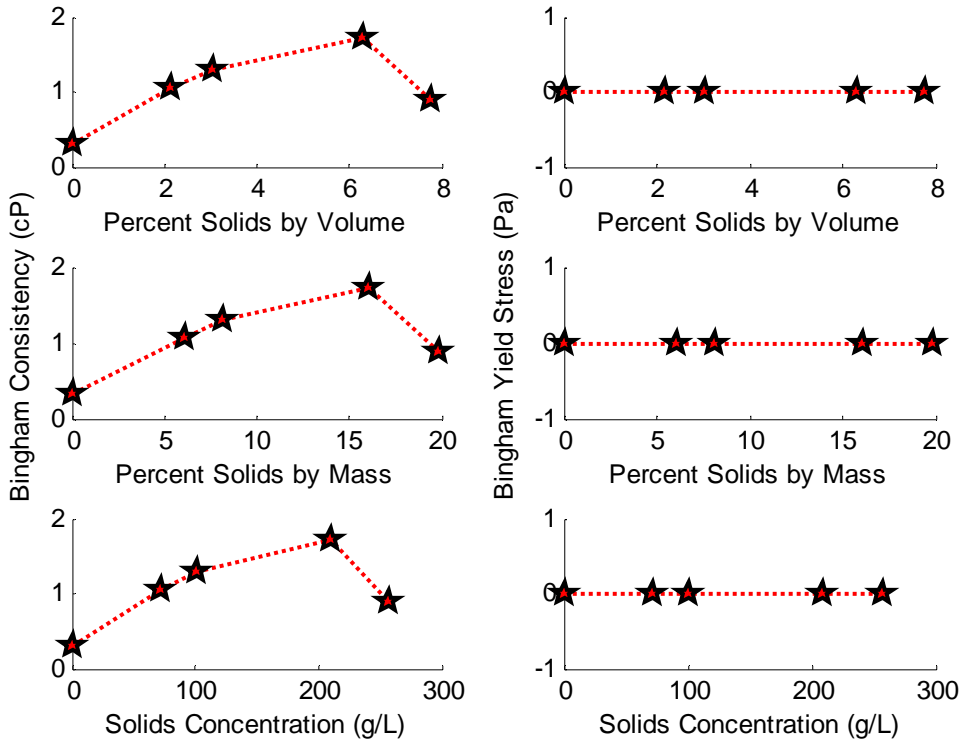
Hanford Tank AY-102 between 20°C and 35°C



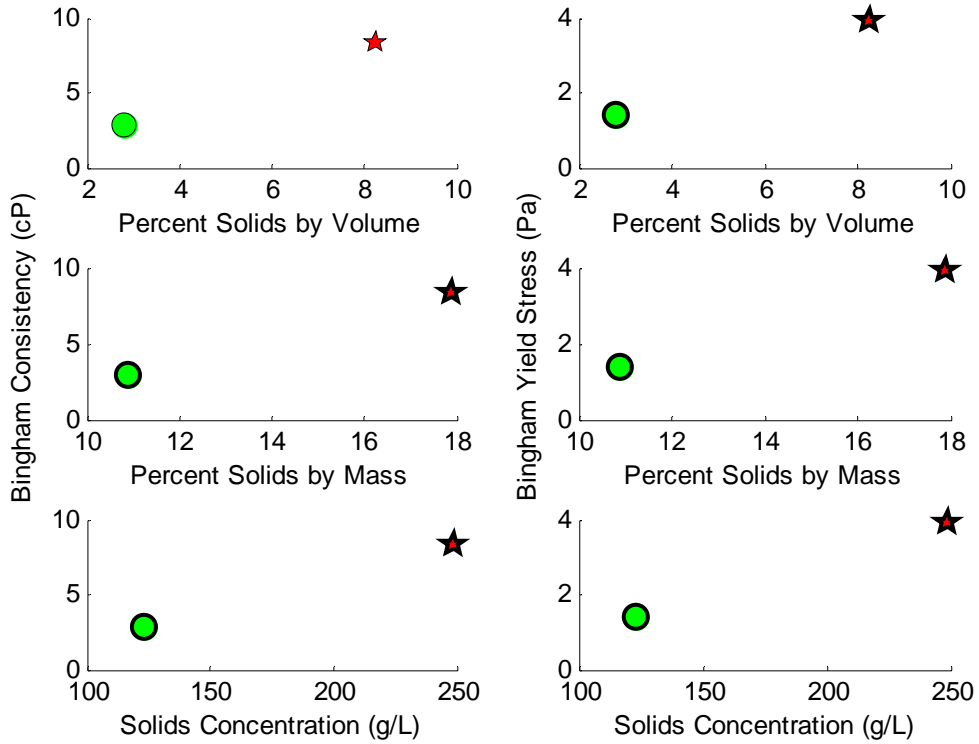
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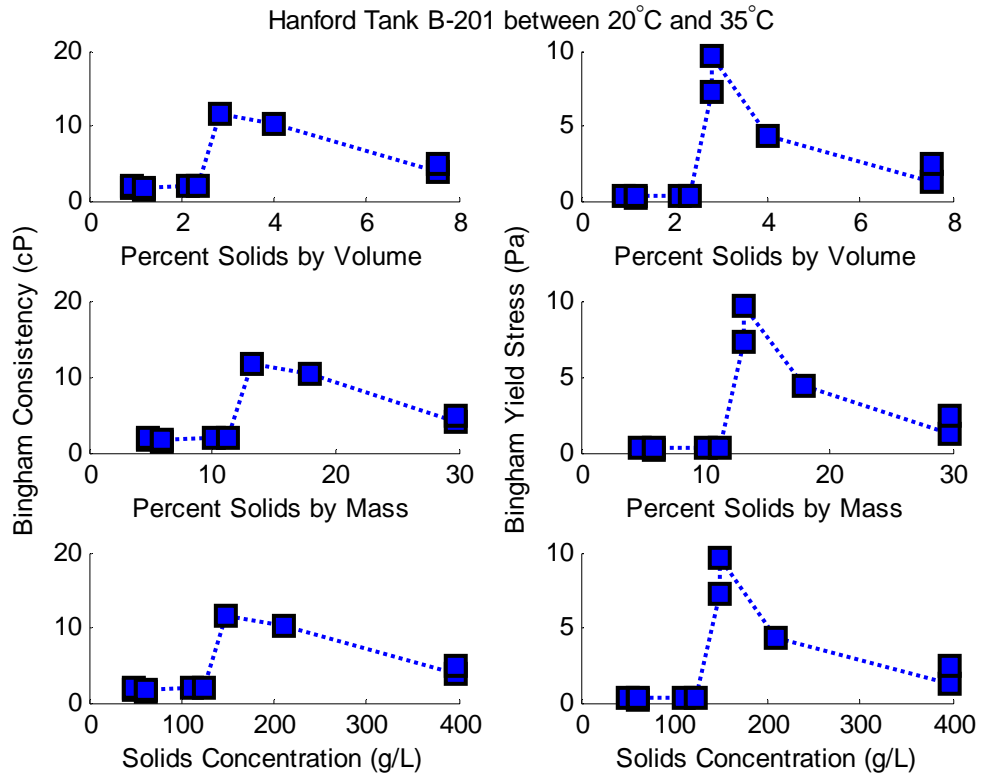
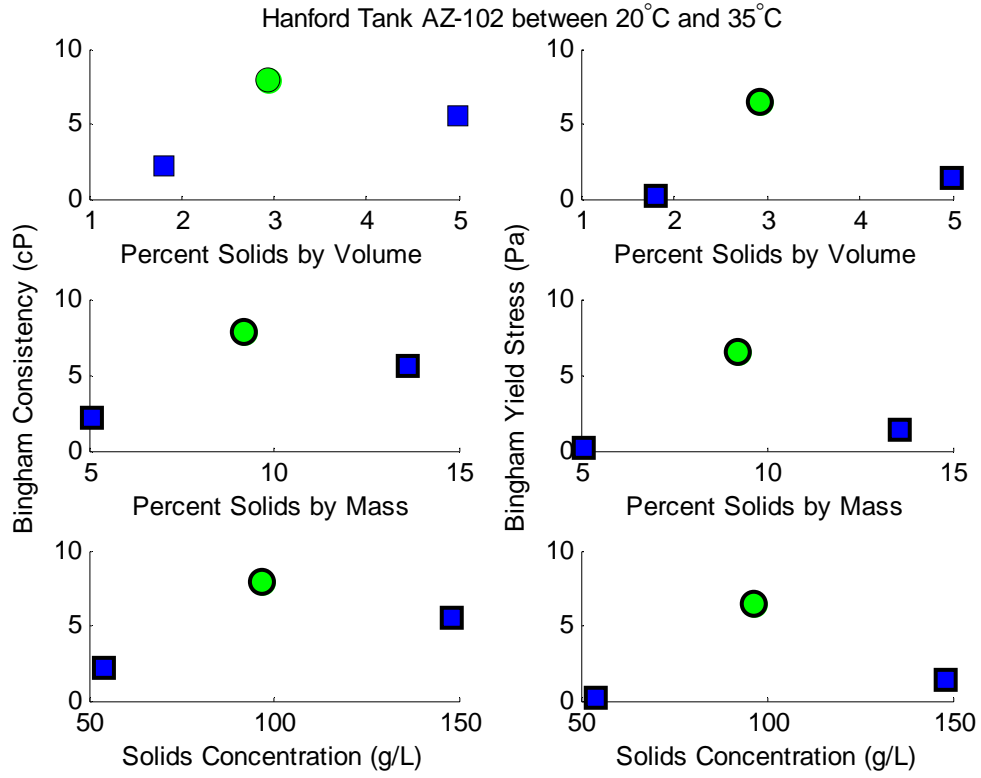


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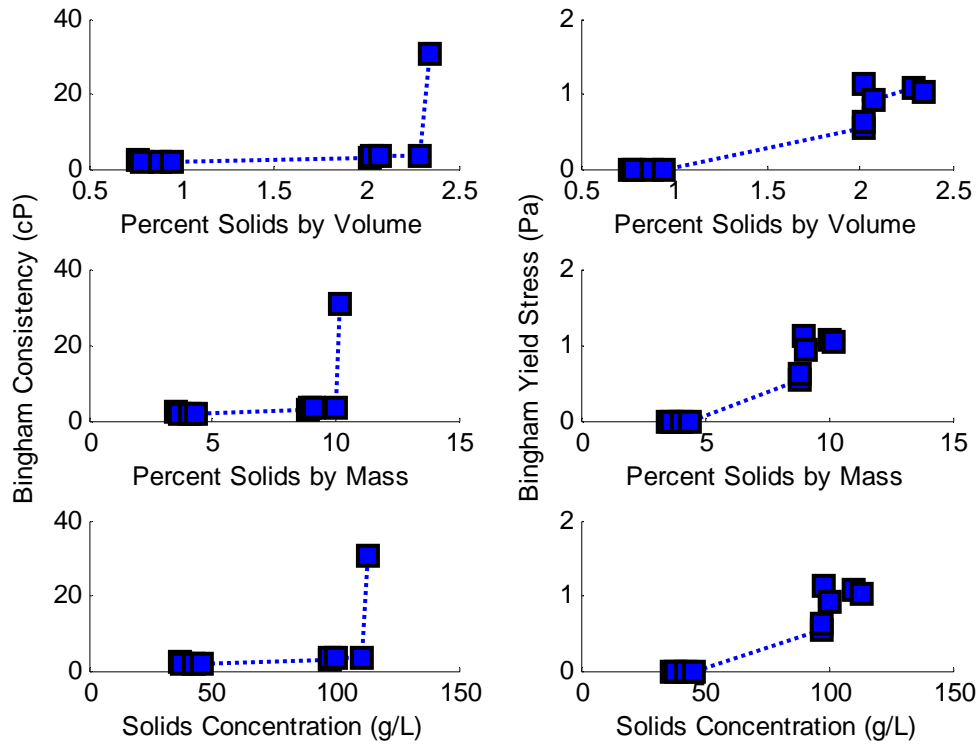


Hanford Tank AZ-101 between 20°C and 35°C

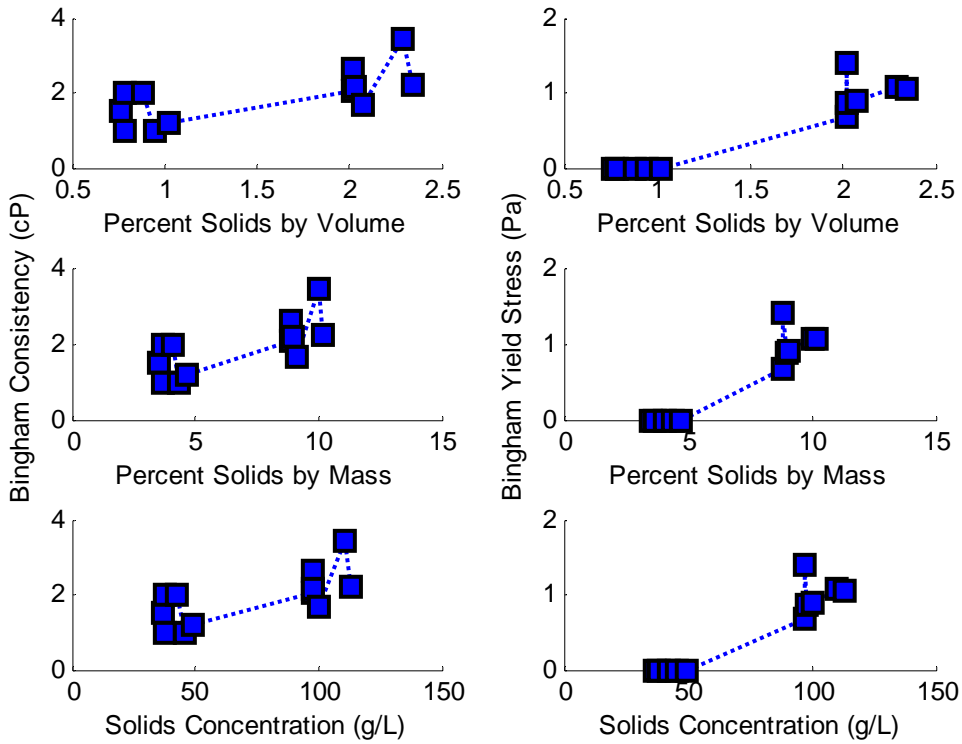


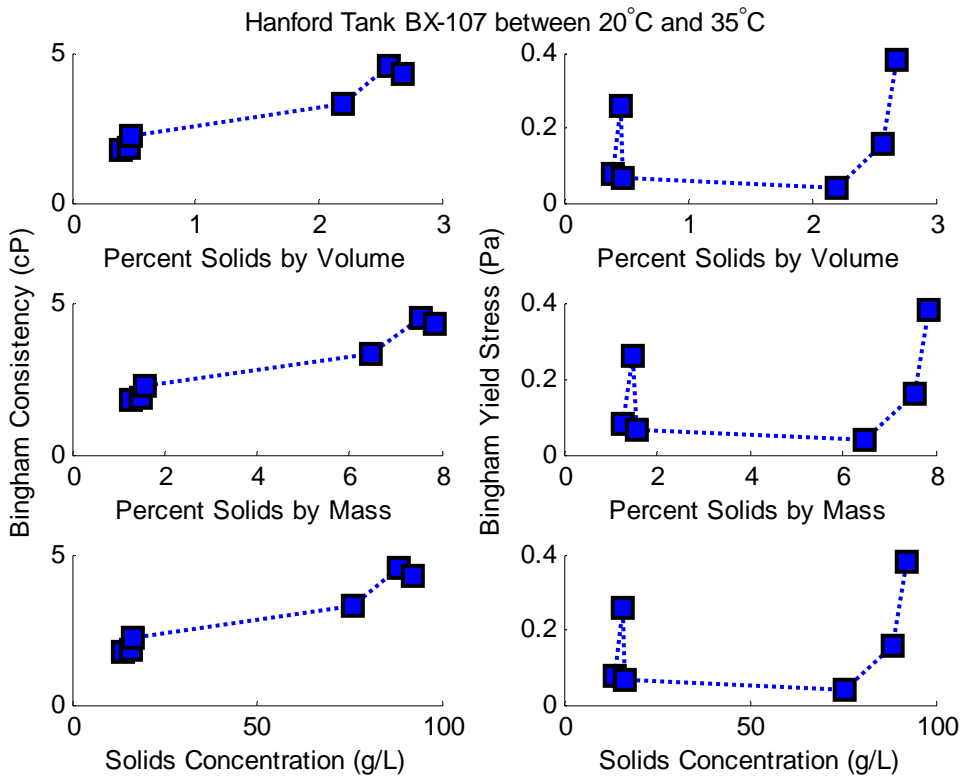
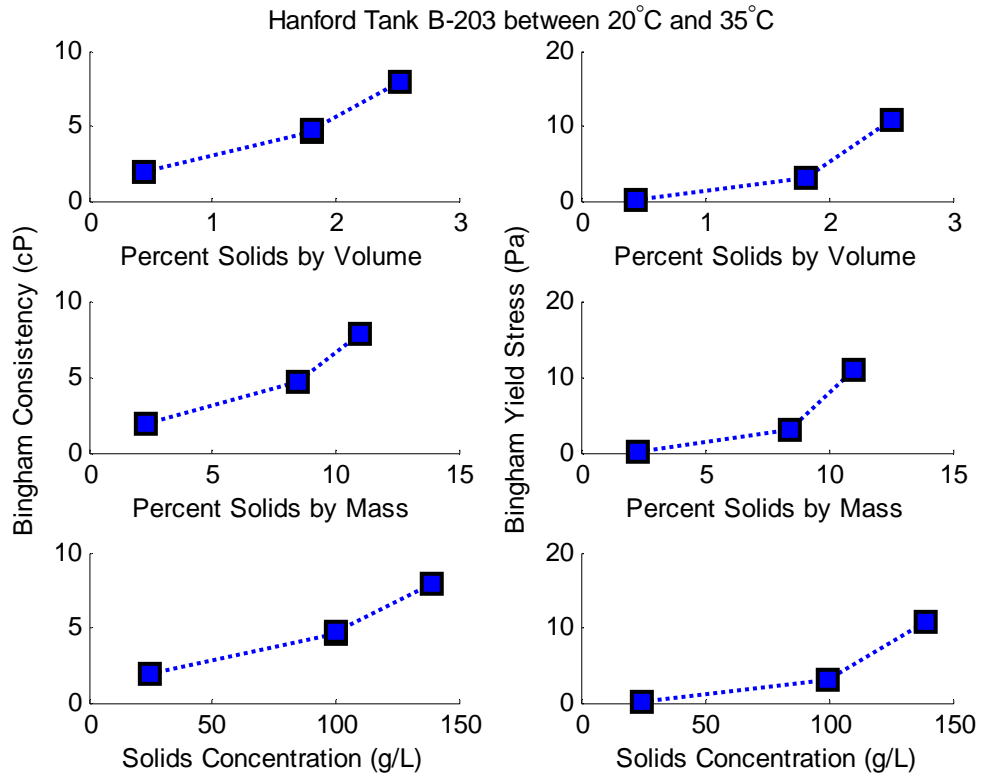


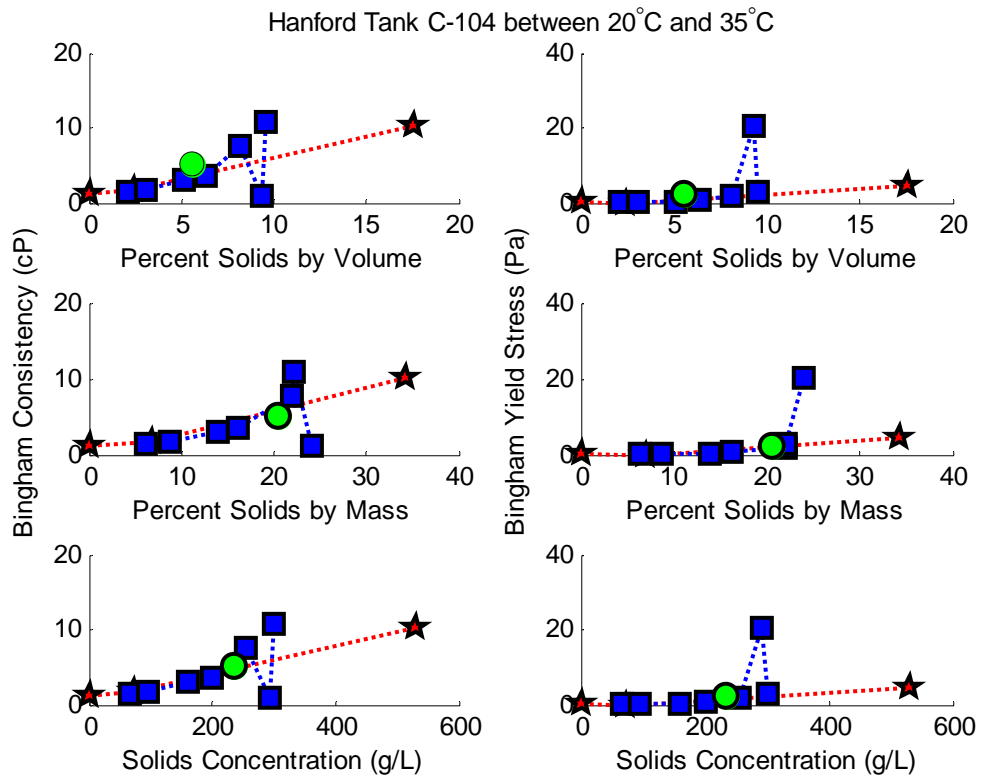
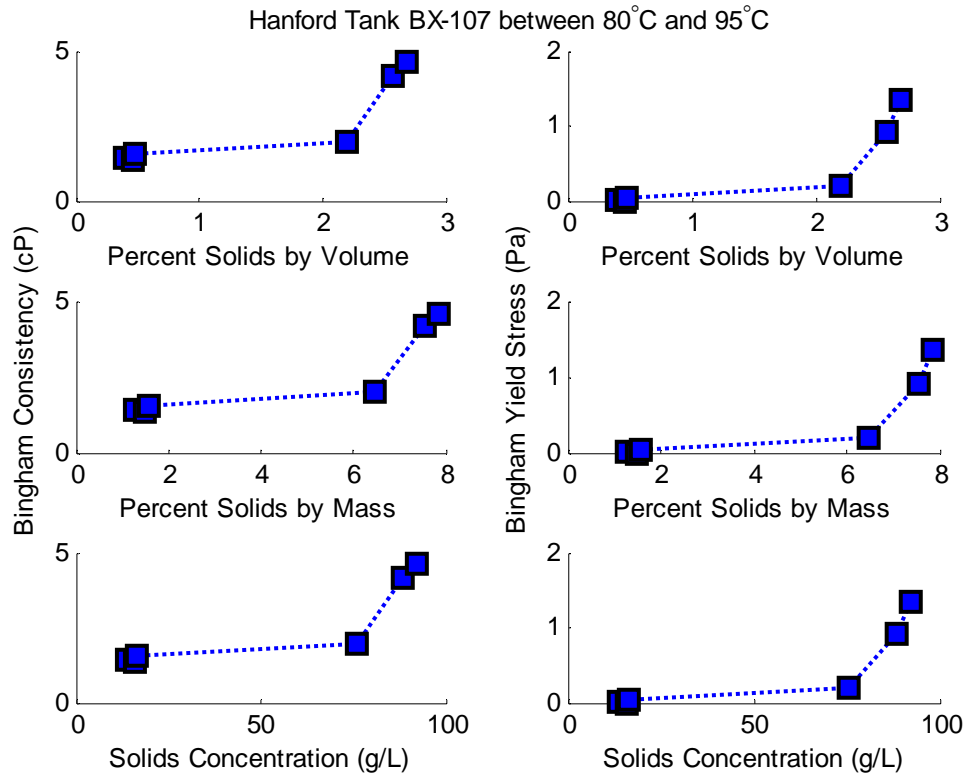
Hanford Tank B-202 between 20°C and 35°C

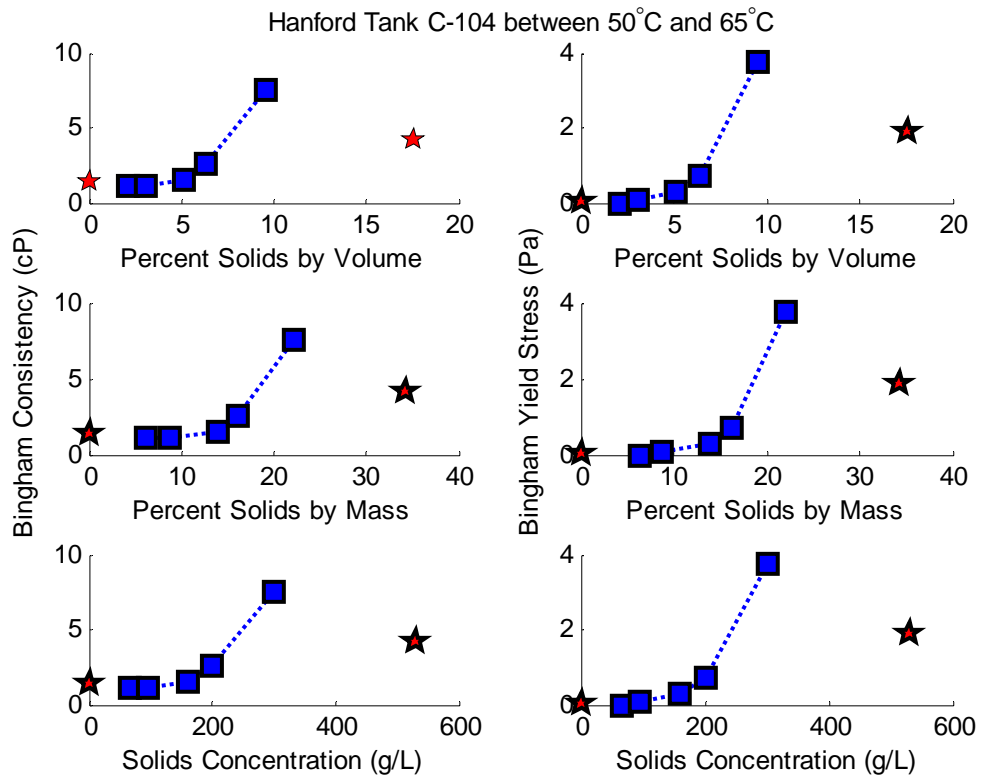
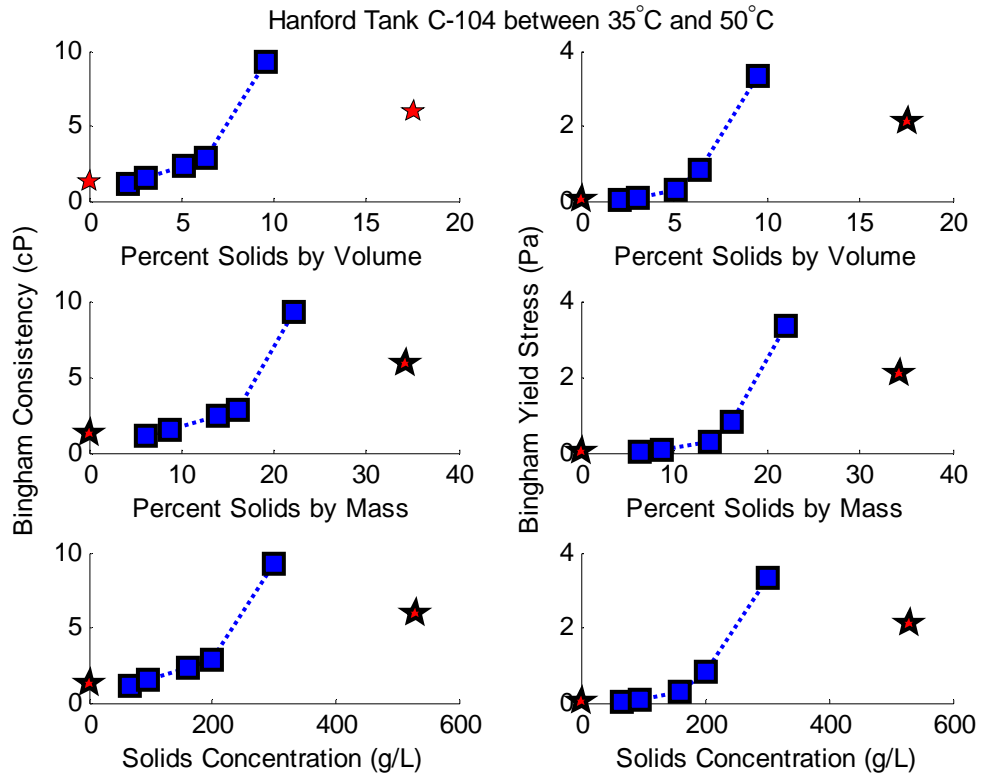


Hanford Tank B-202 between 80°C and 95°C



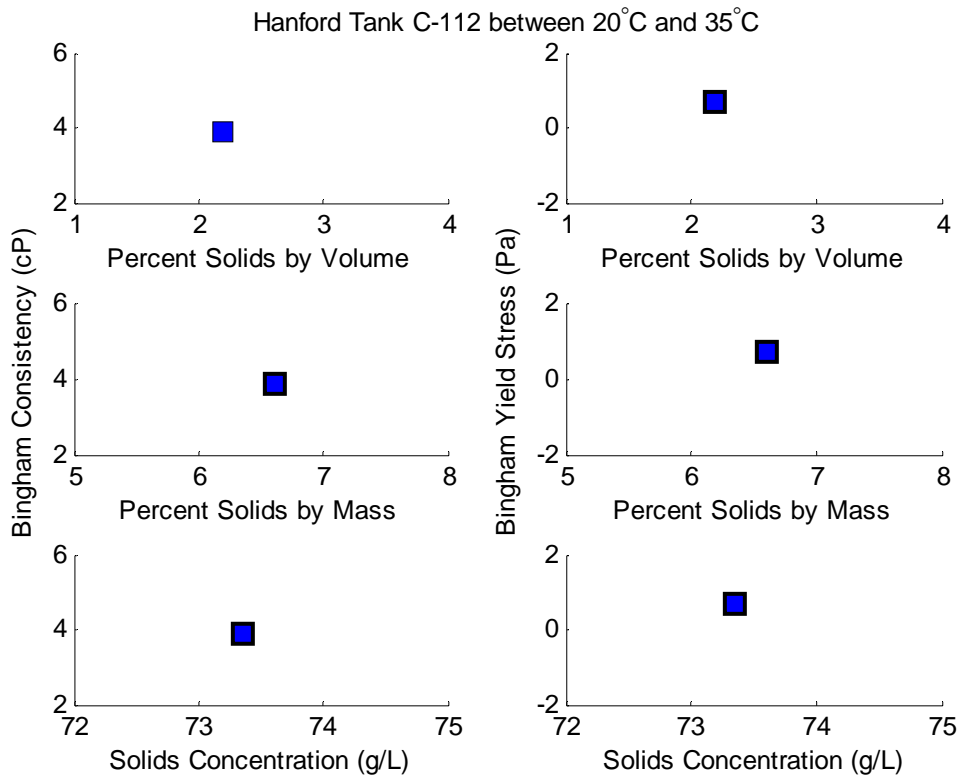
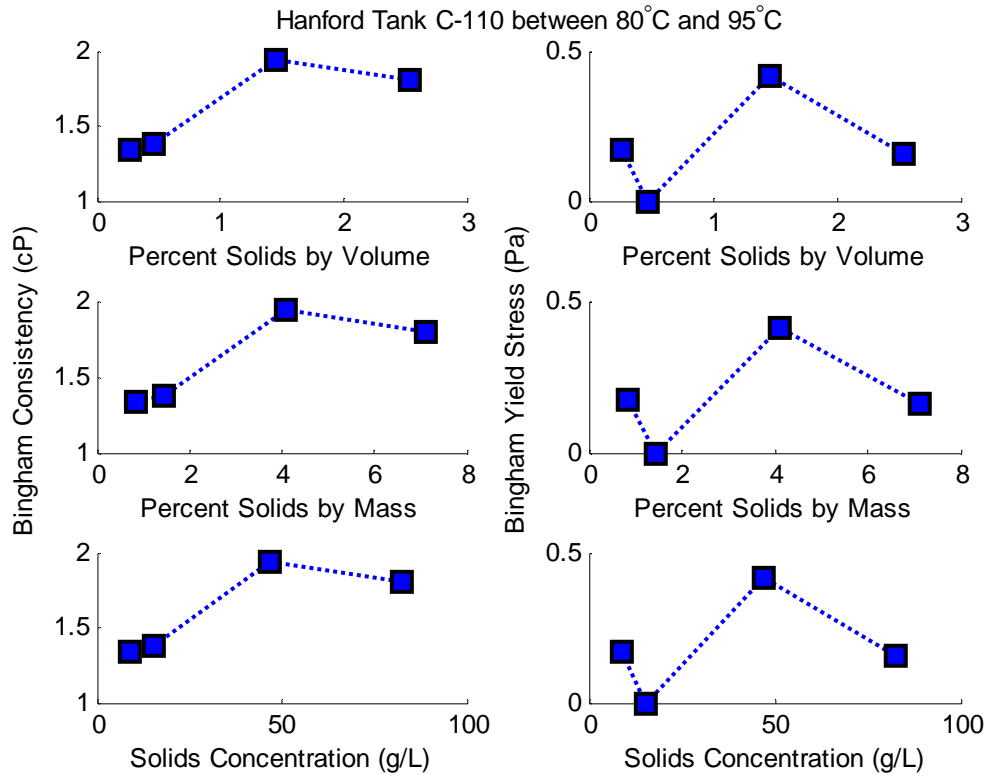




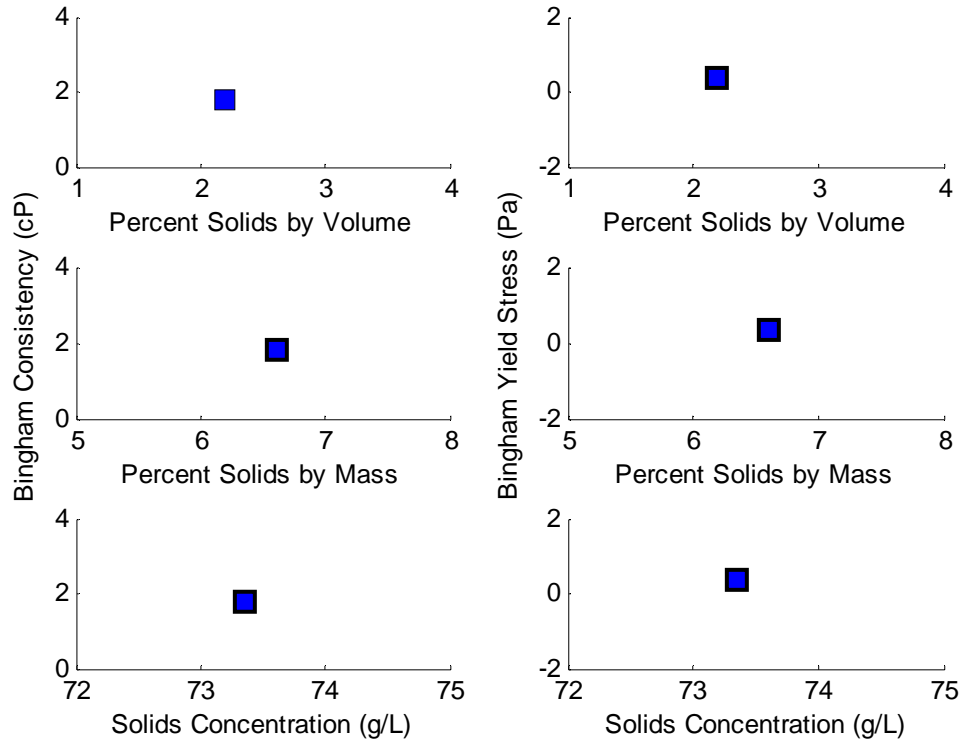




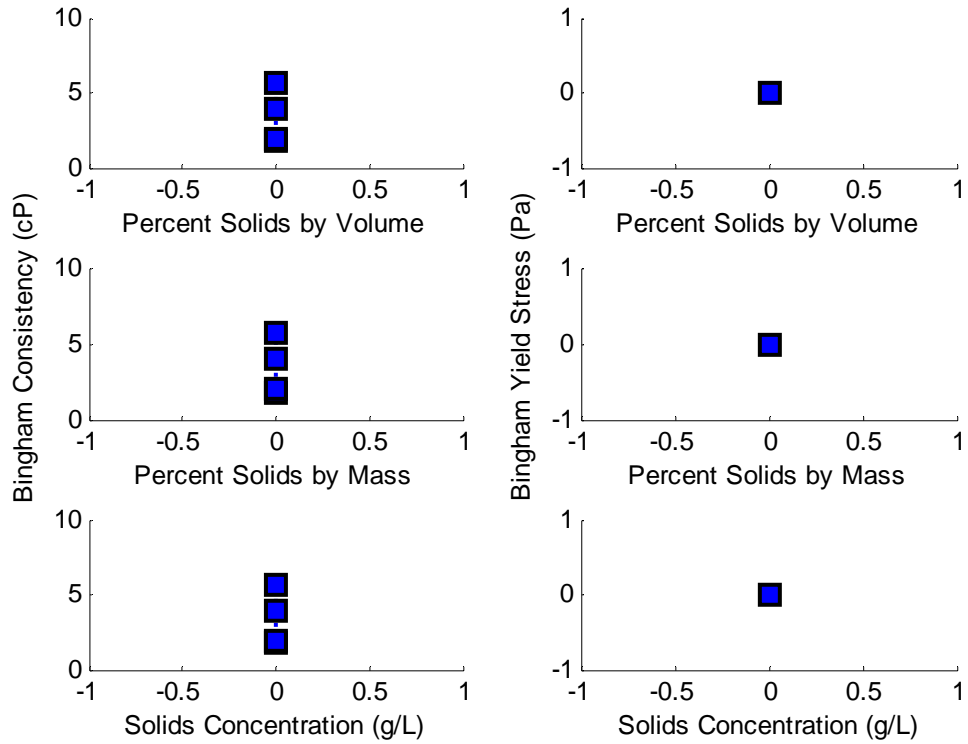


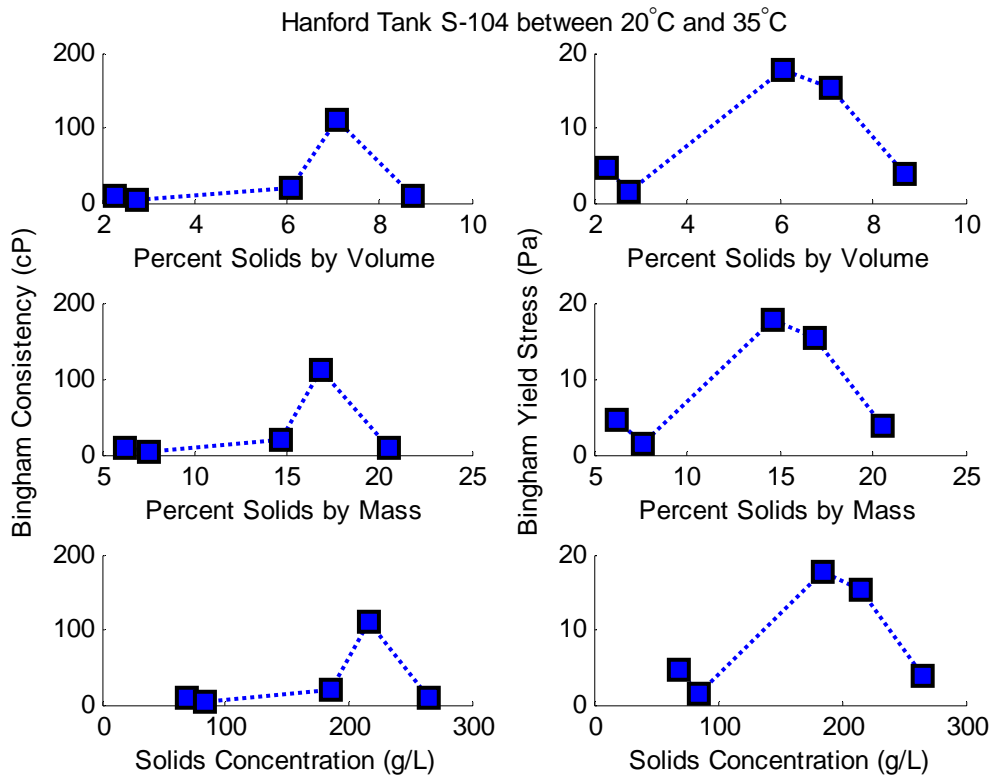
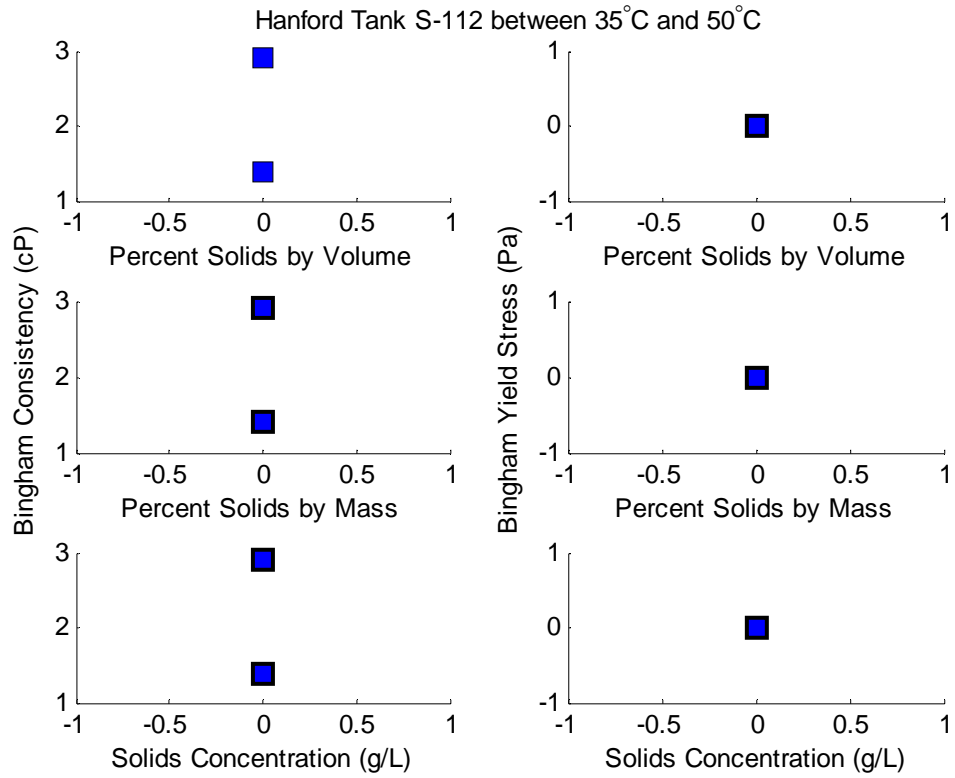


Hanford Tank C-112 between 80°C and 95°C

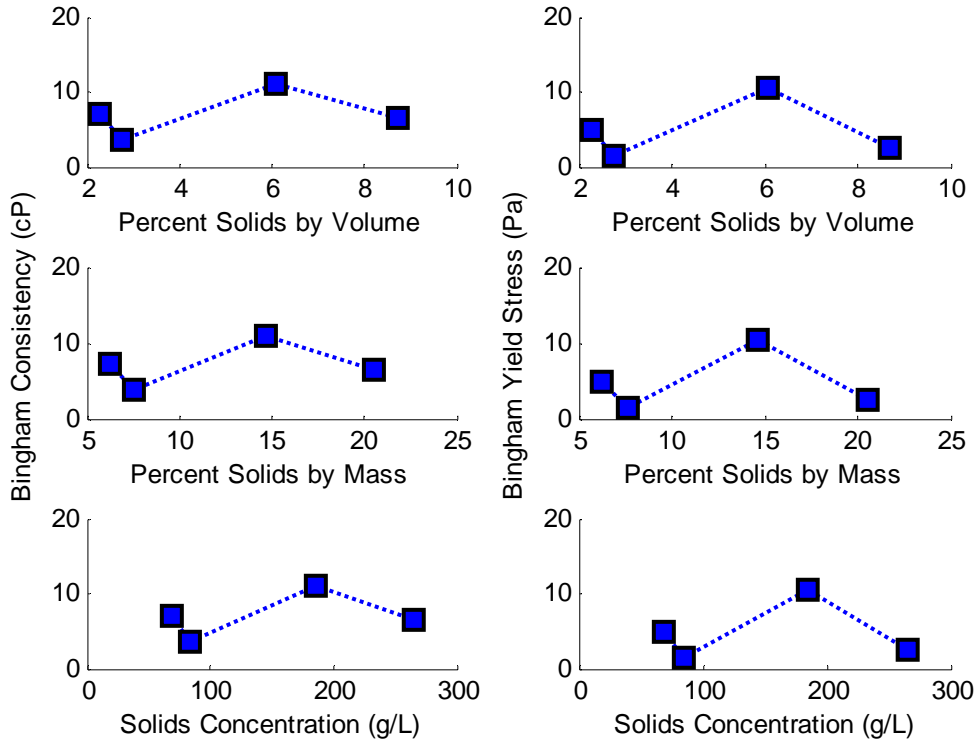


Hanford Tank S-112 between 20°C and 35°C

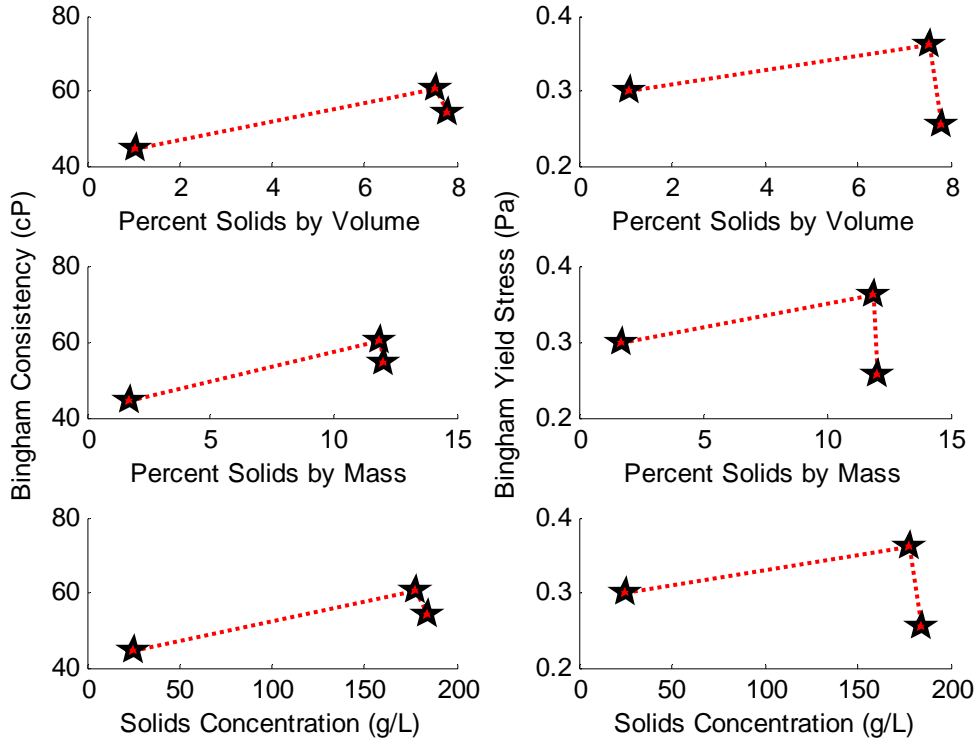


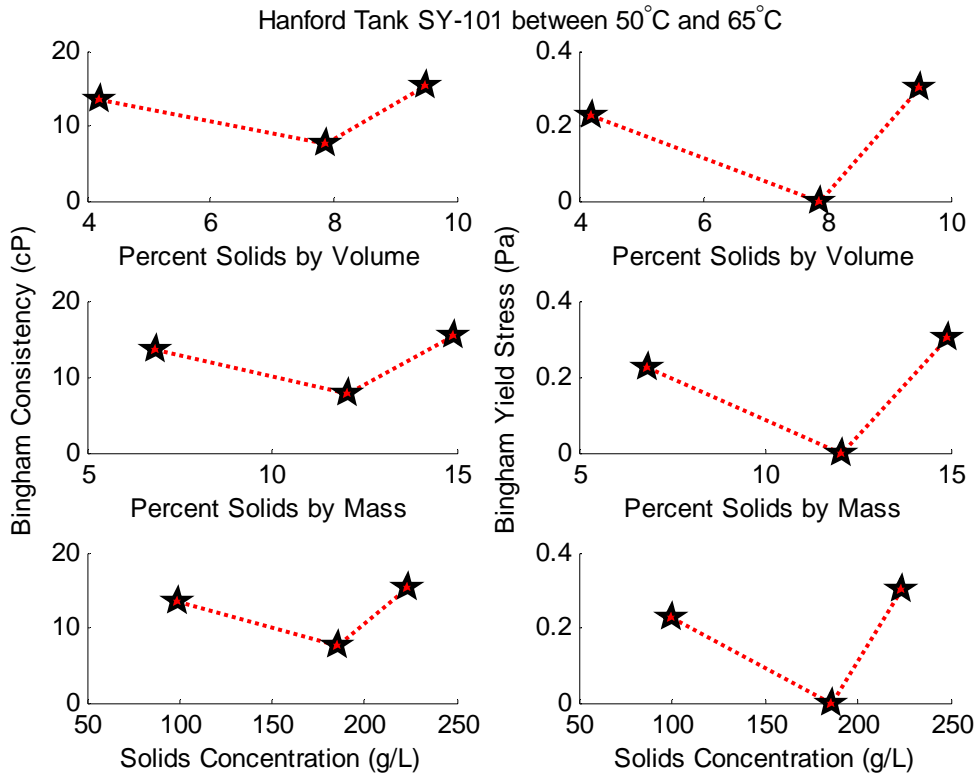
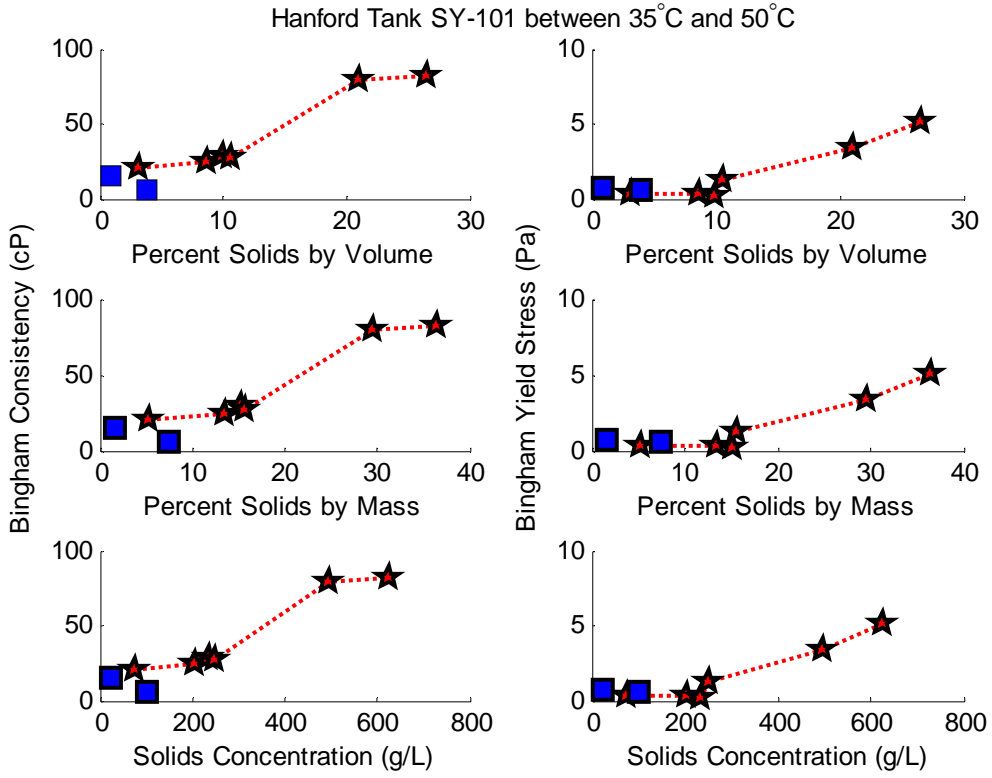


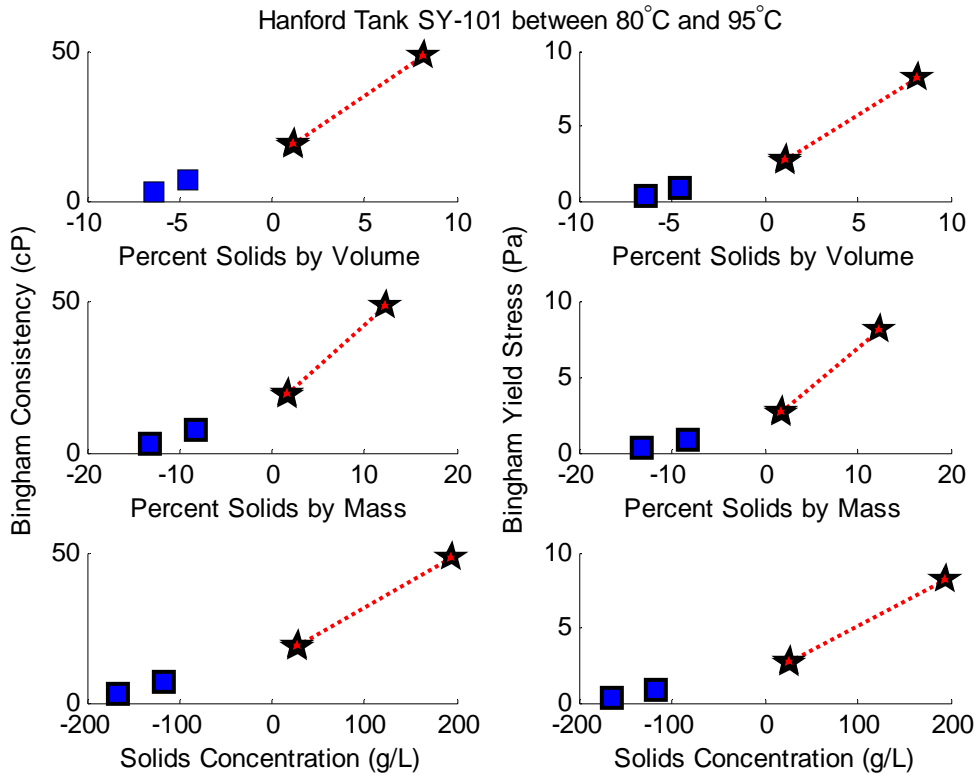
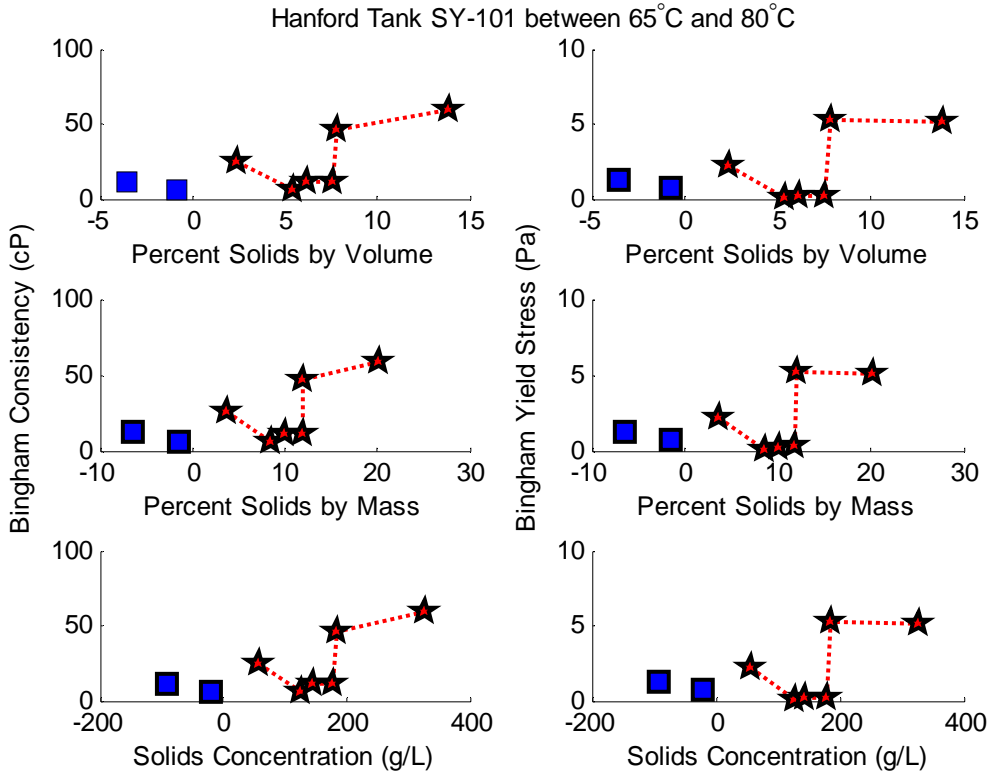
Hanford Tank S-104 between 80°C and 95°C



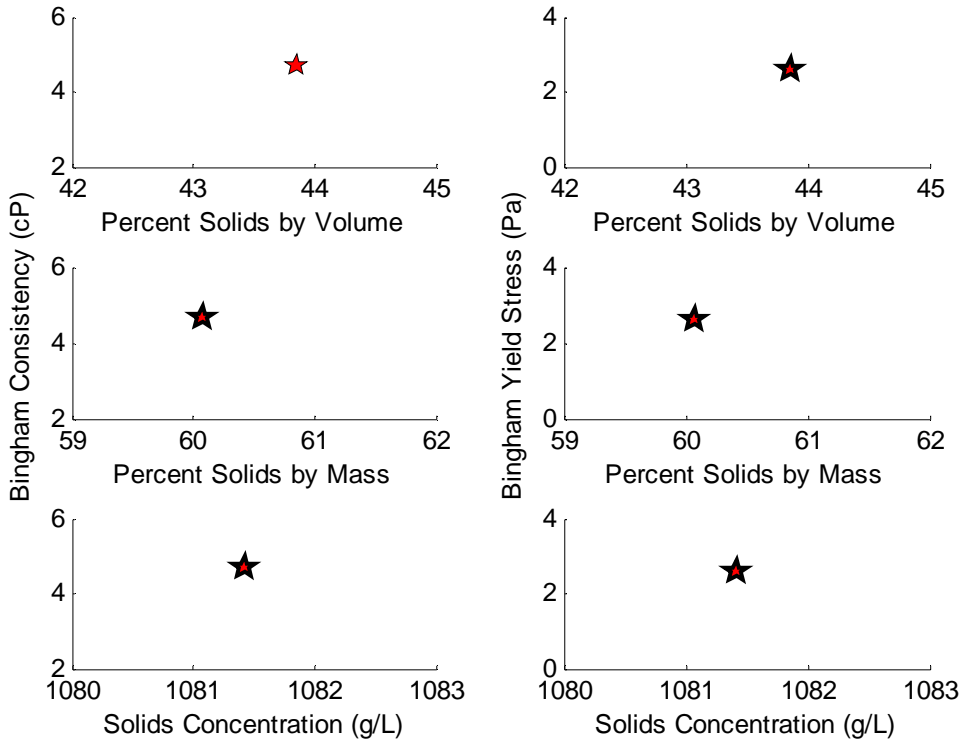
Hanford Tank SY-101 between 20°C and 35°C



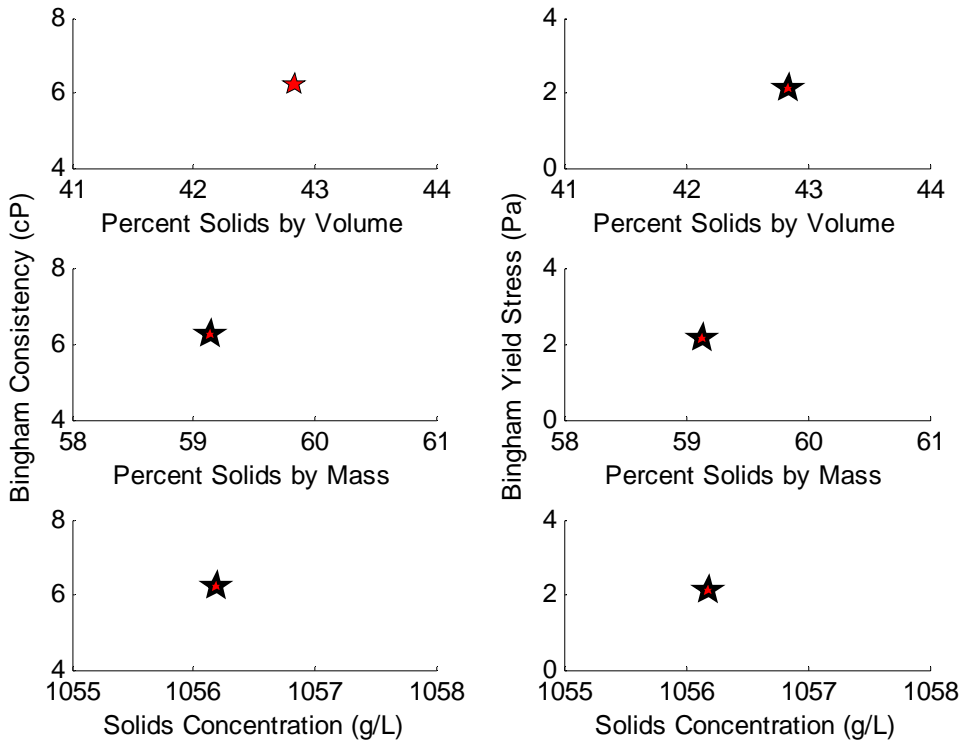




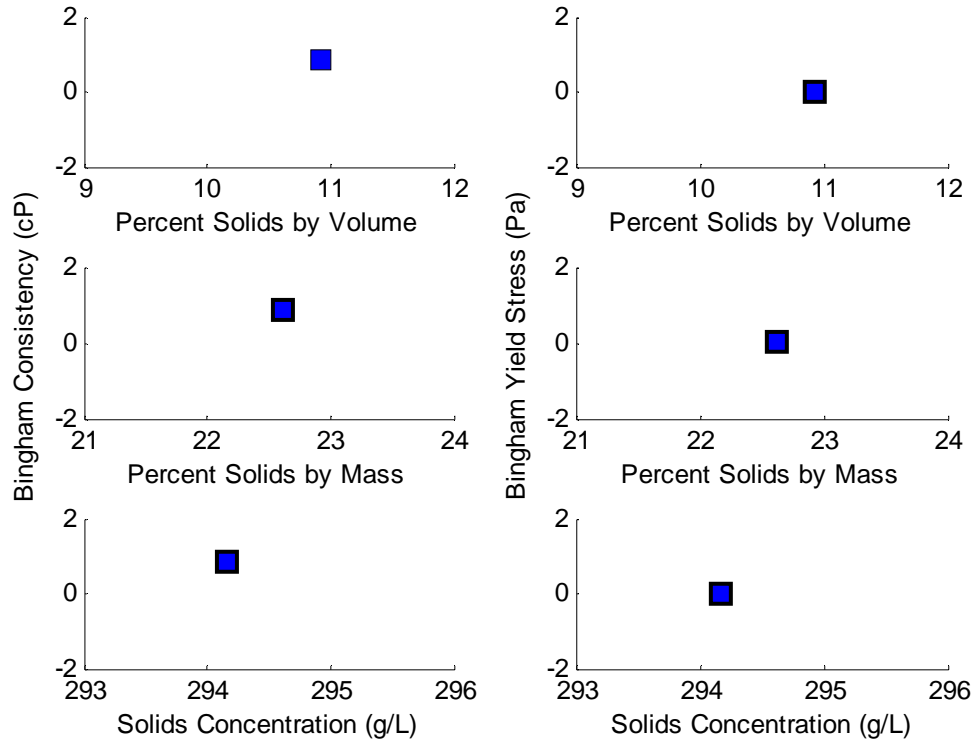
Hanford Tank SY-102 between 20°C and 35°C



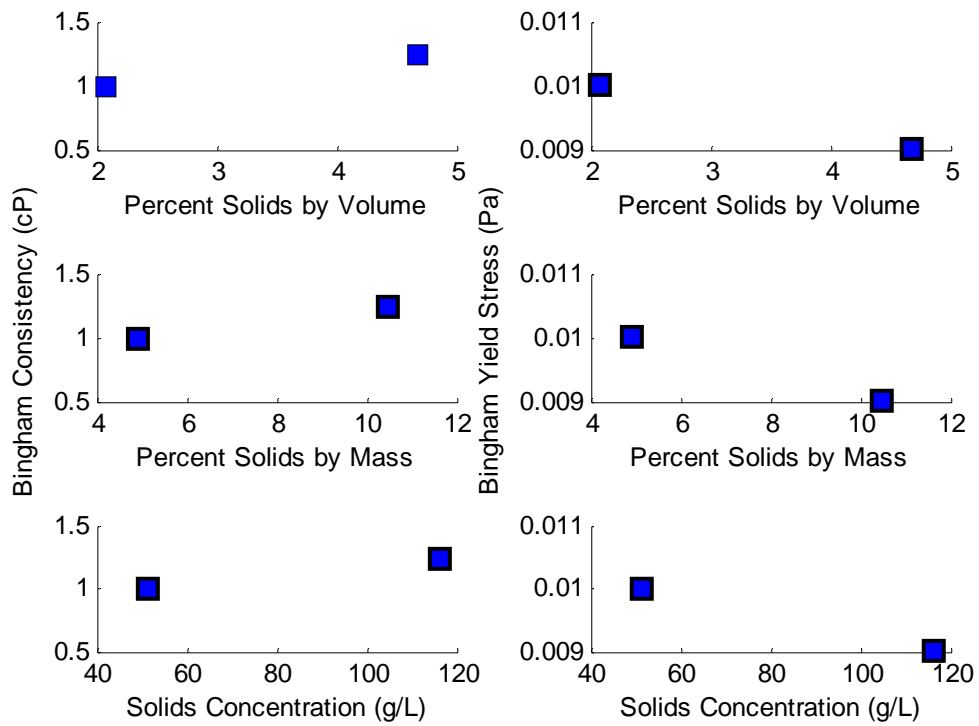
Hanford Tank SY-102 between 35°C and 50°C



Hanford Tank SY-102 between 50°C and 65°C

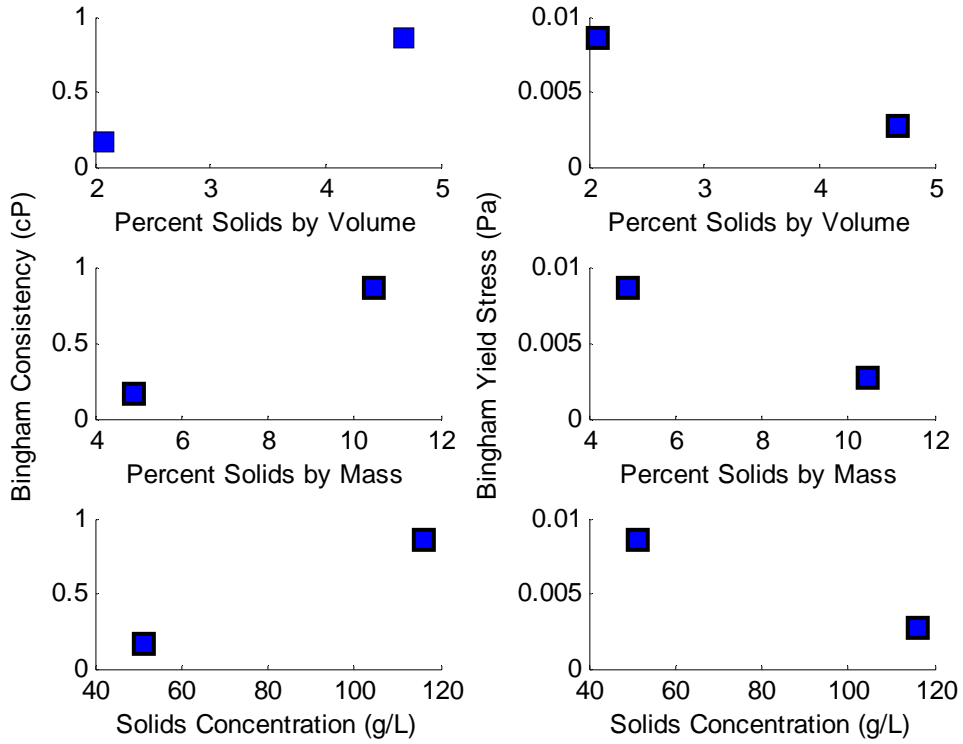


Hanford Tank T-102 between 20°C and 35°C

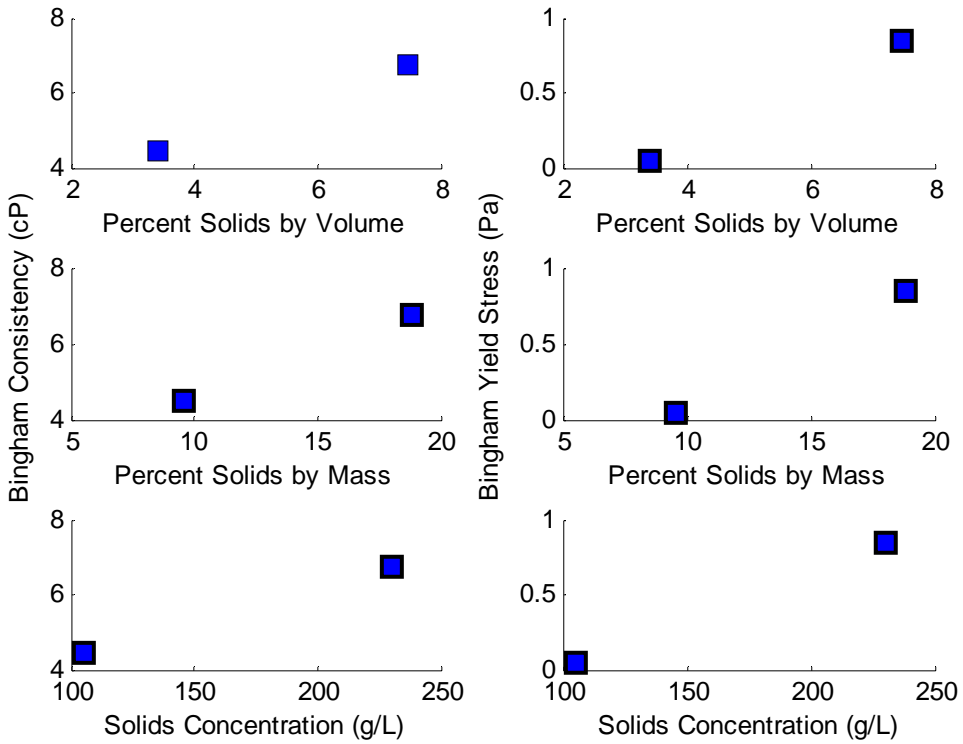




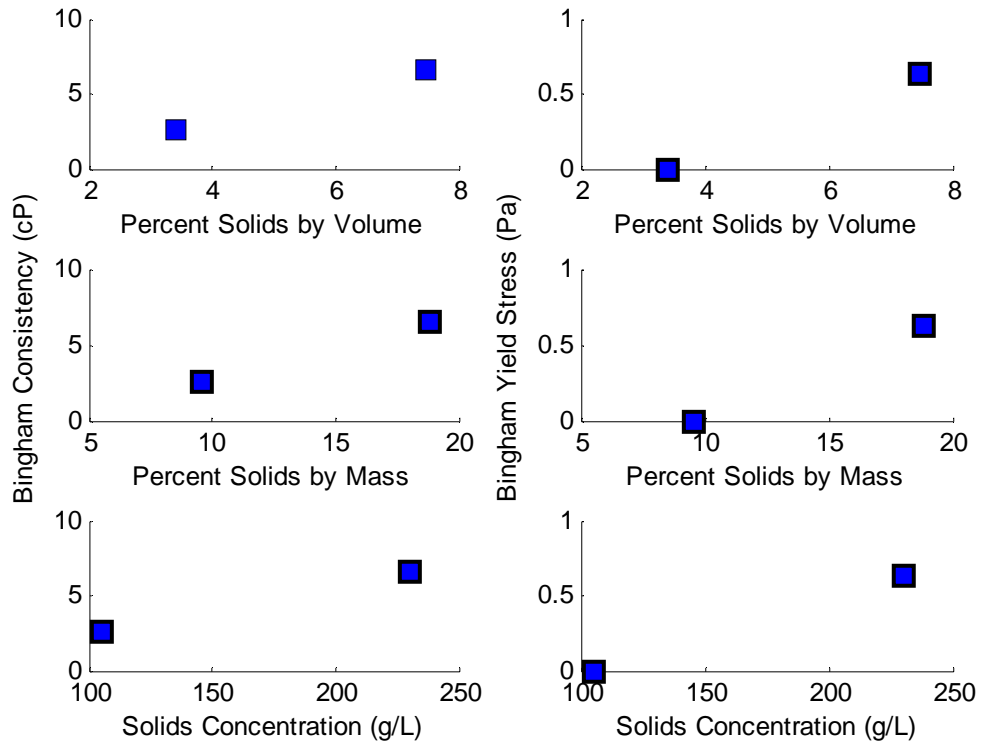
Hanford Tank T-102 between 80°C and 95°C



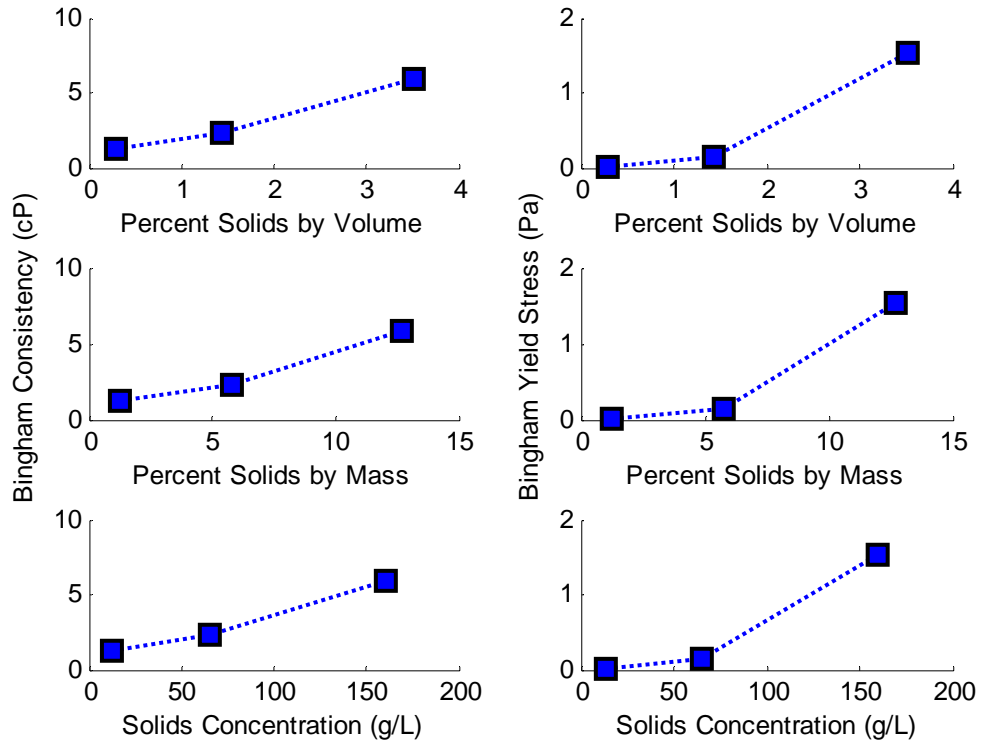
Hanford Tank T-107 between 20°C and 35°C



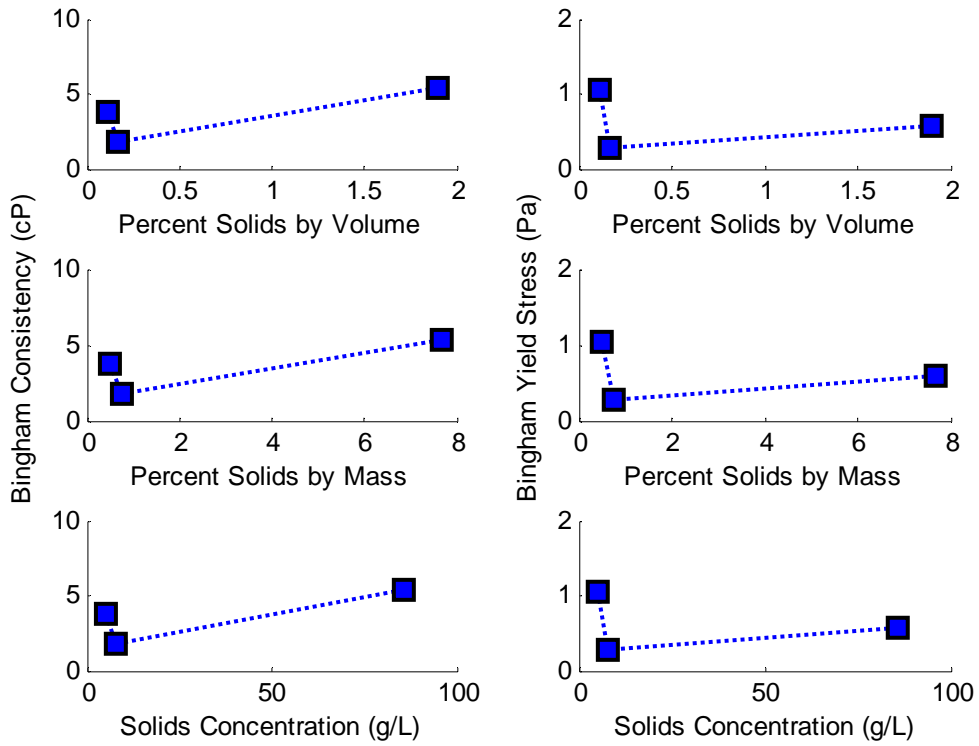
Hanford Tank T-107 between 80°C and 95°C



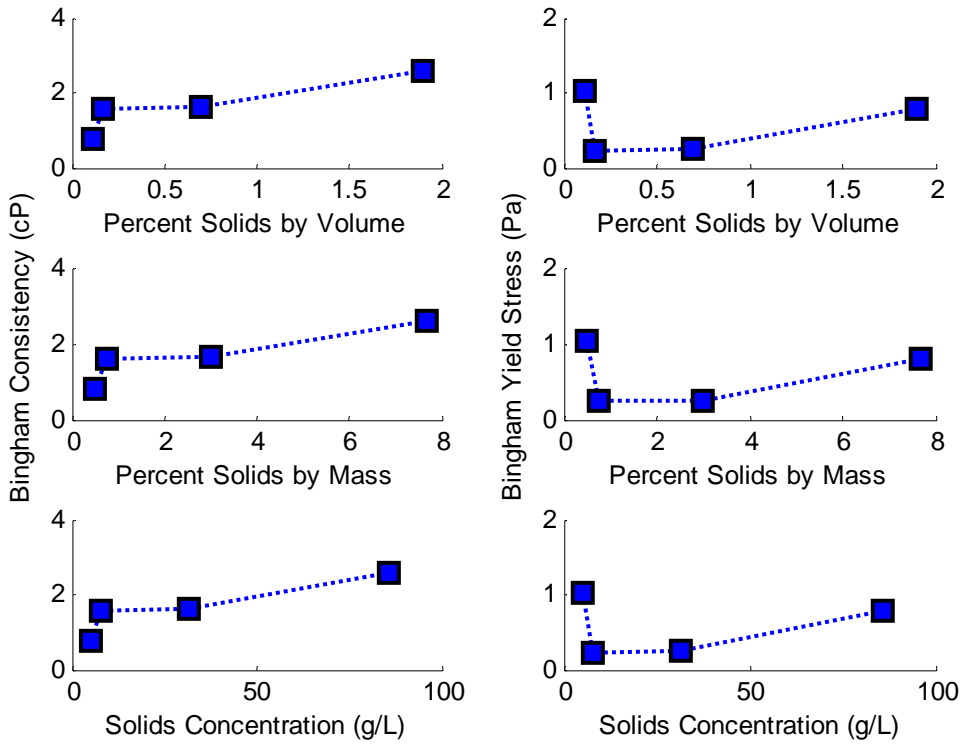
Hanford Tank T-110 between 20°C and 35°C

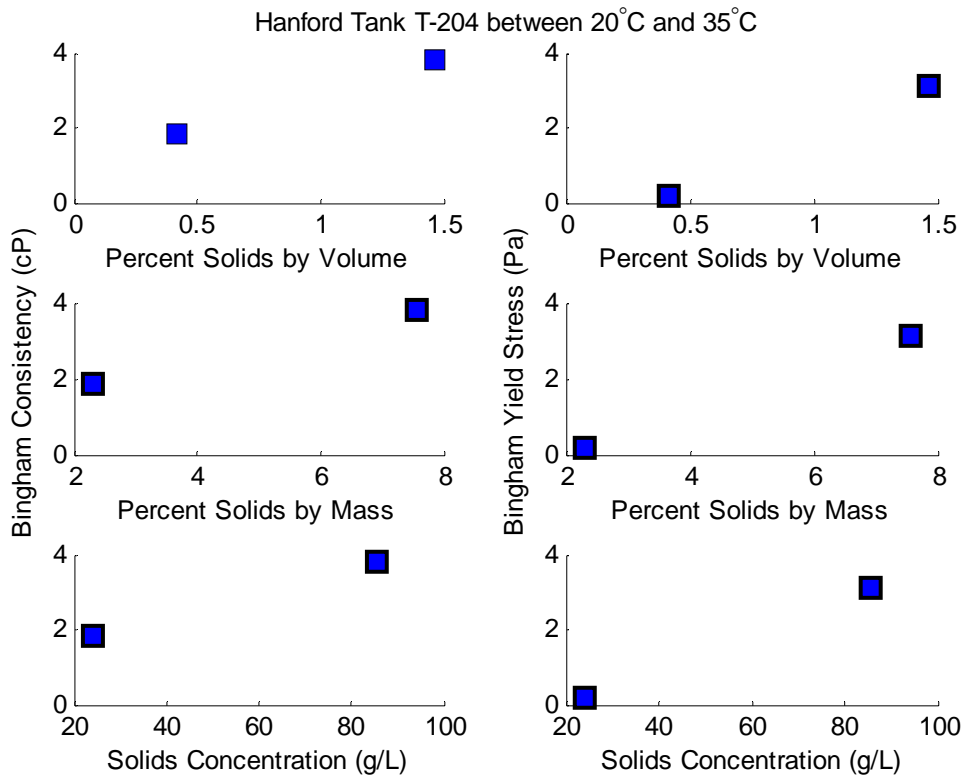
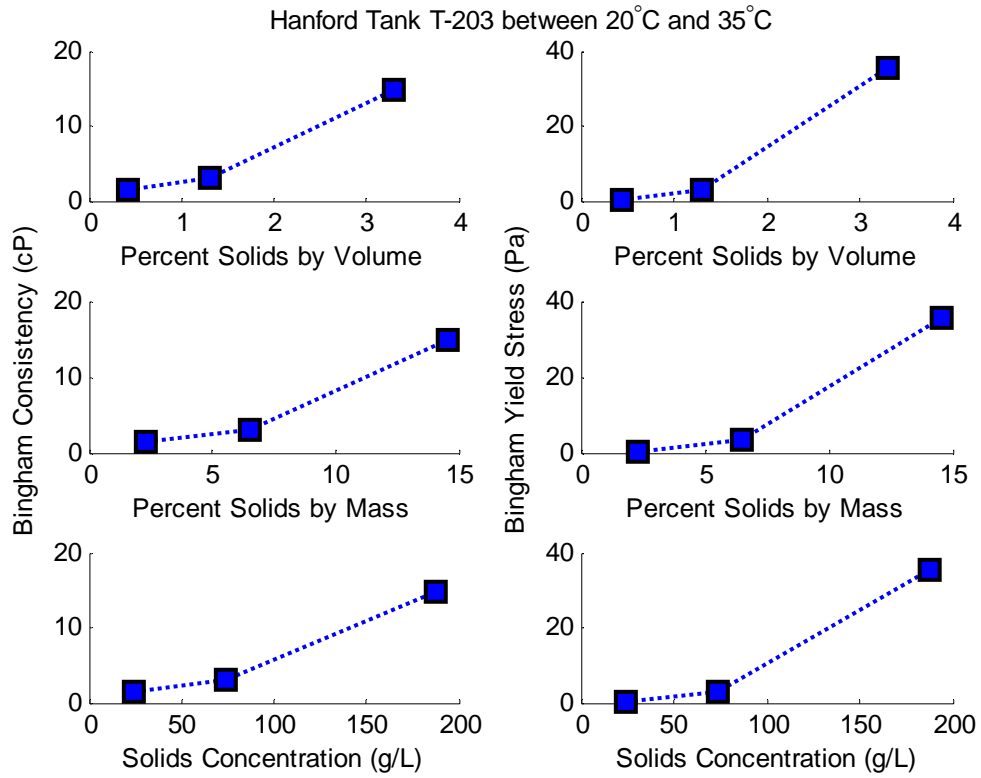


Hanford Tank T-111 between 20°C and 35°C



Hanford Tank T-111 between 80°C and 95°C



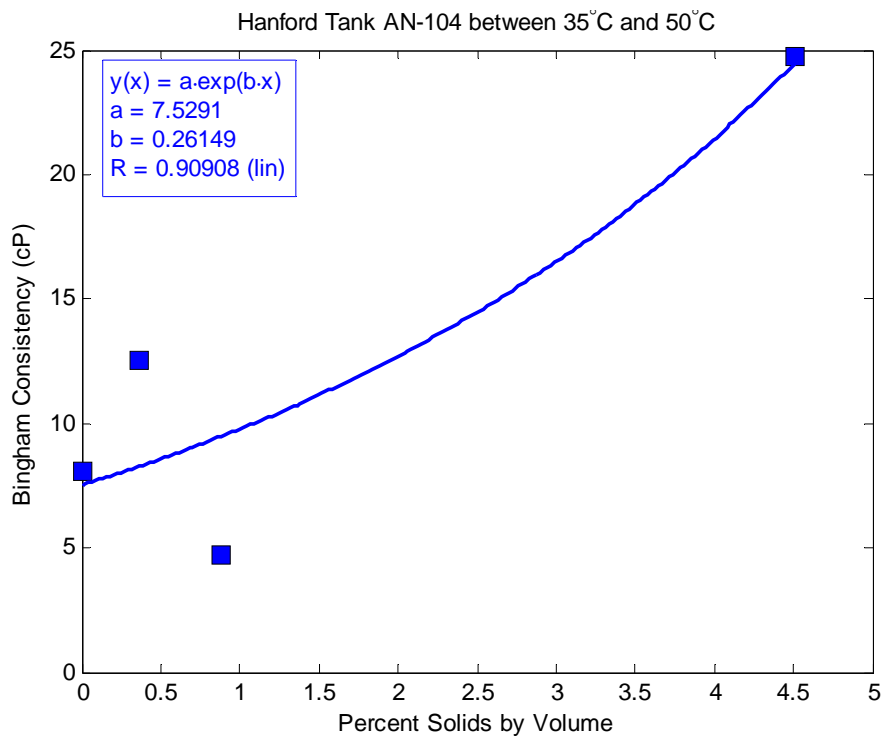
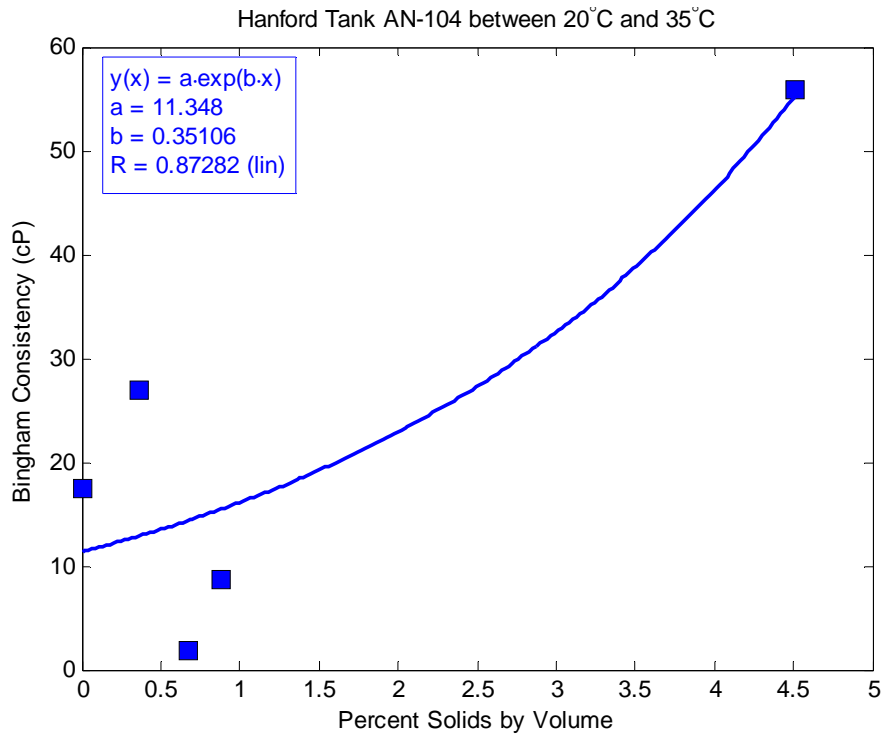


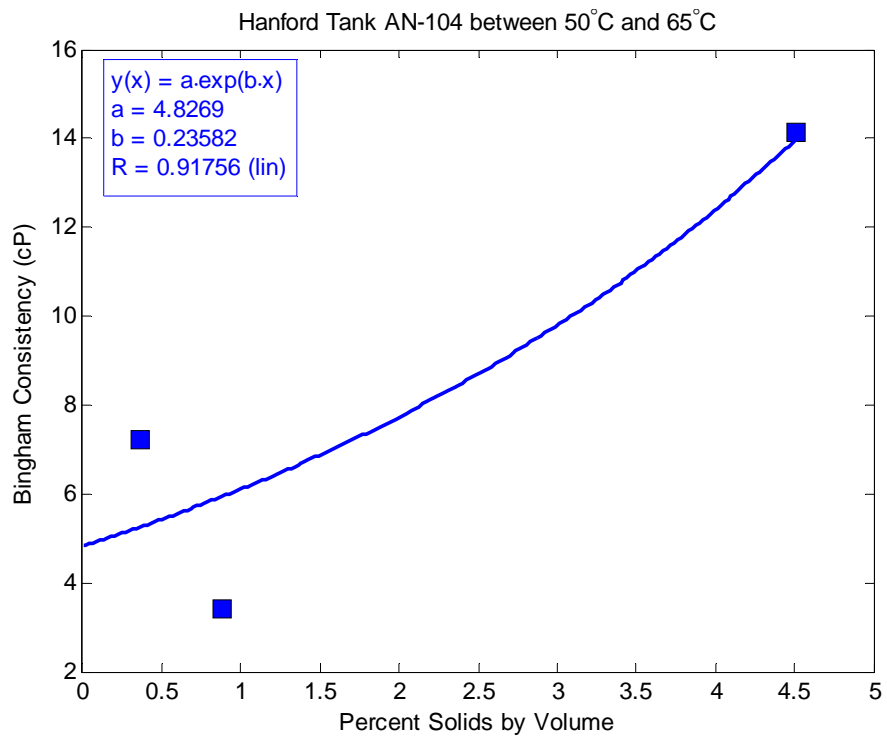
## **Appendix C**

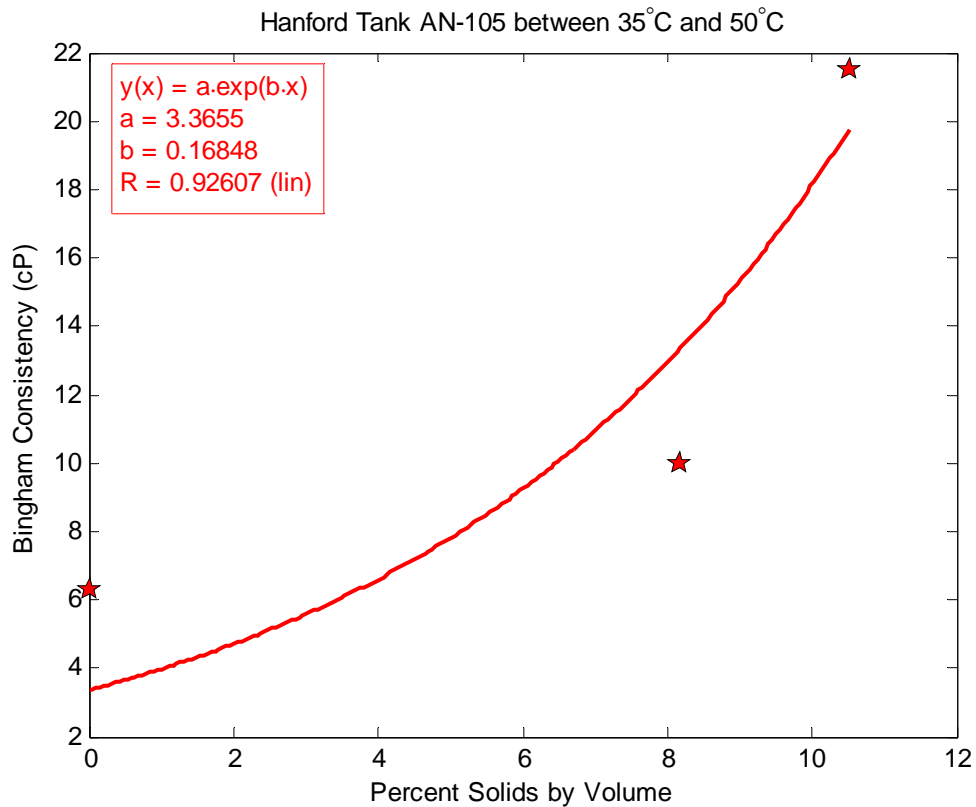
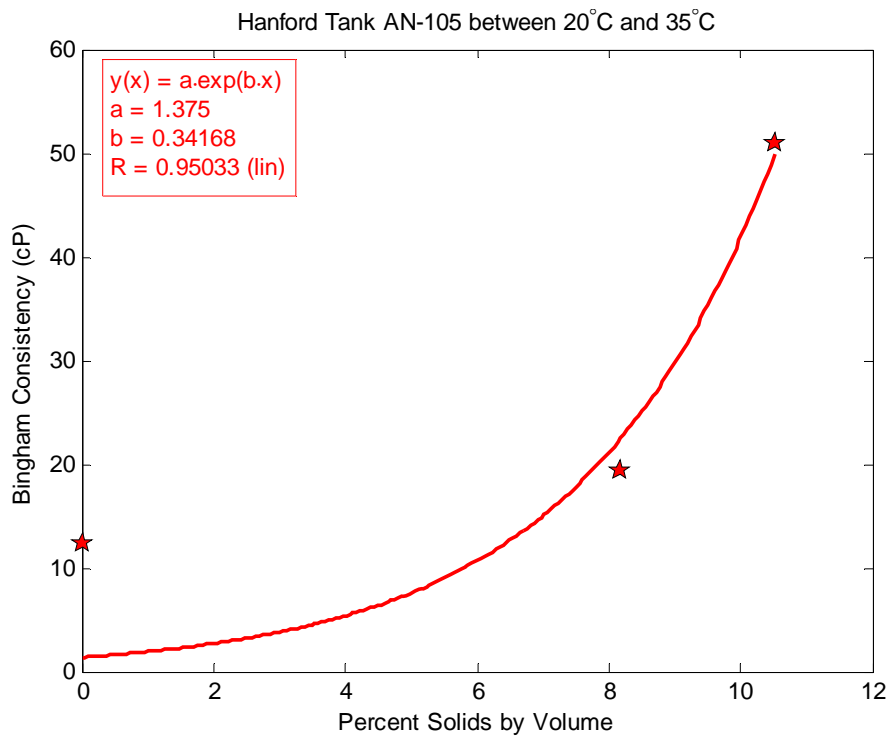
### **Correlations of the Bingham Plastic Model Parameters with Solids Content**

# Appendix C – Correlations of the Bingham Plastic Model Parameters with Solids Content

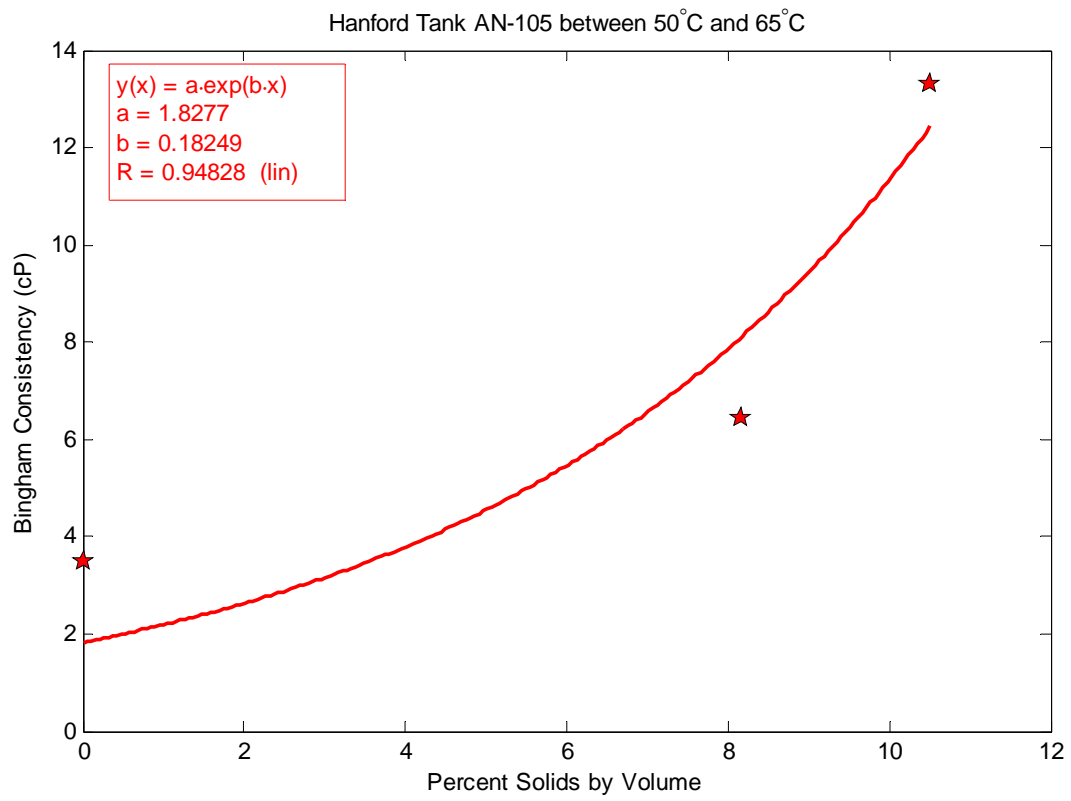
In the figures in this appendix, the stars = as-received tank waste; squares = water added as diluent; and circles = post washing and caustic.



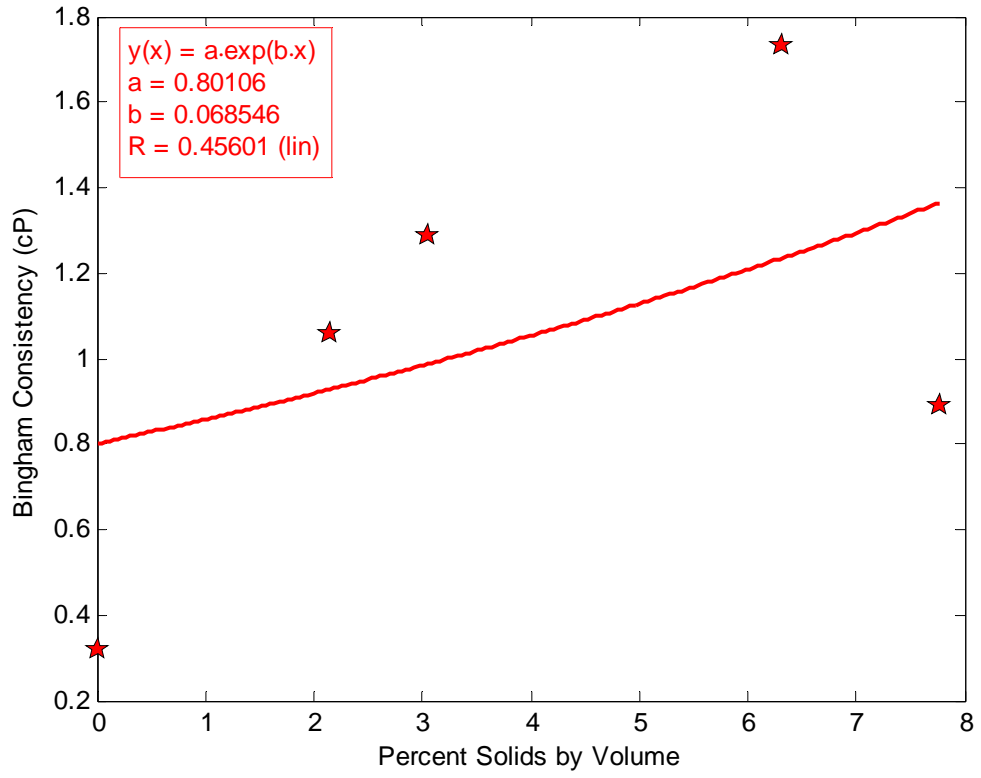




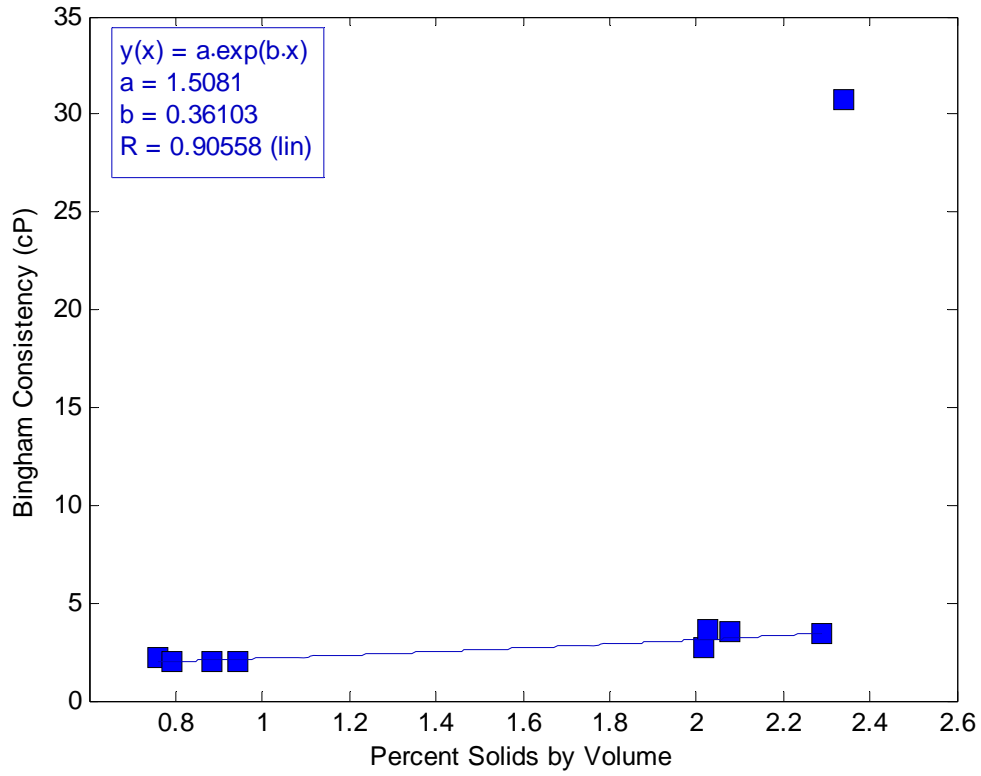




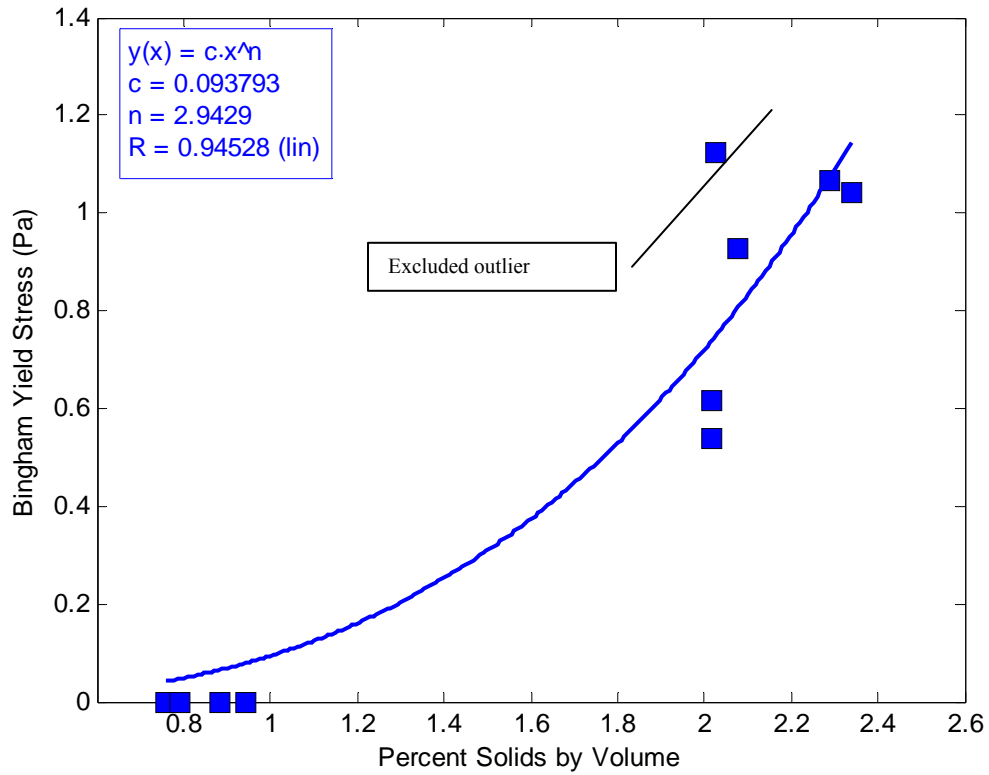
Hanford Tank AY-102 between 50°C and 65°C

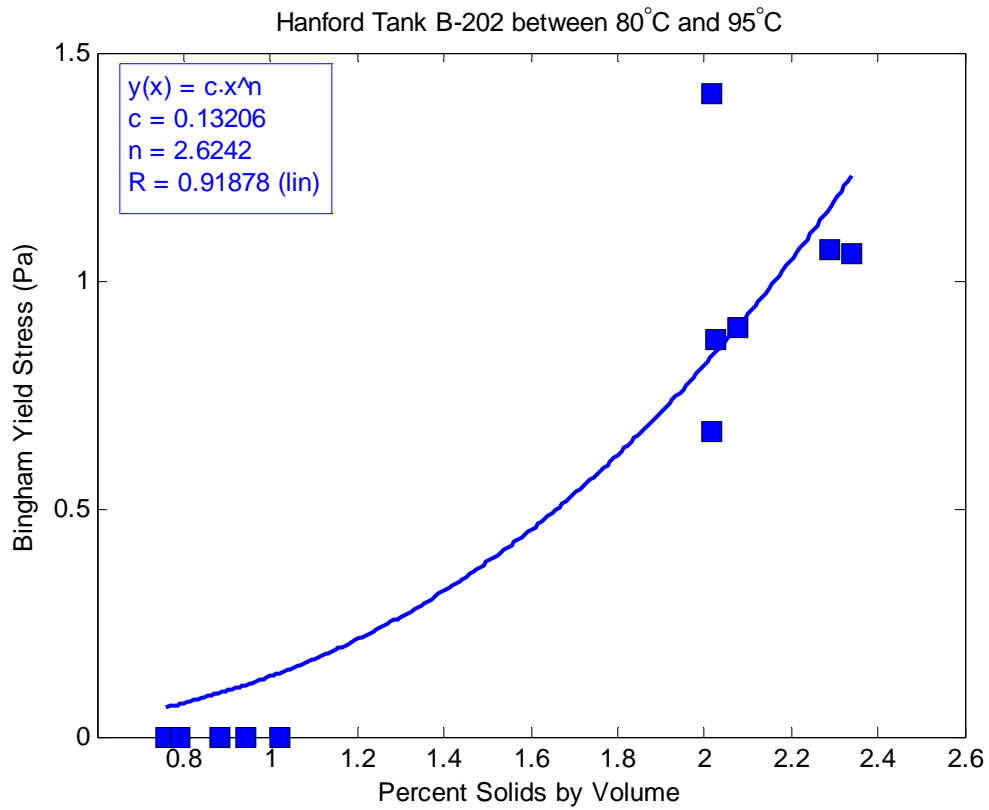
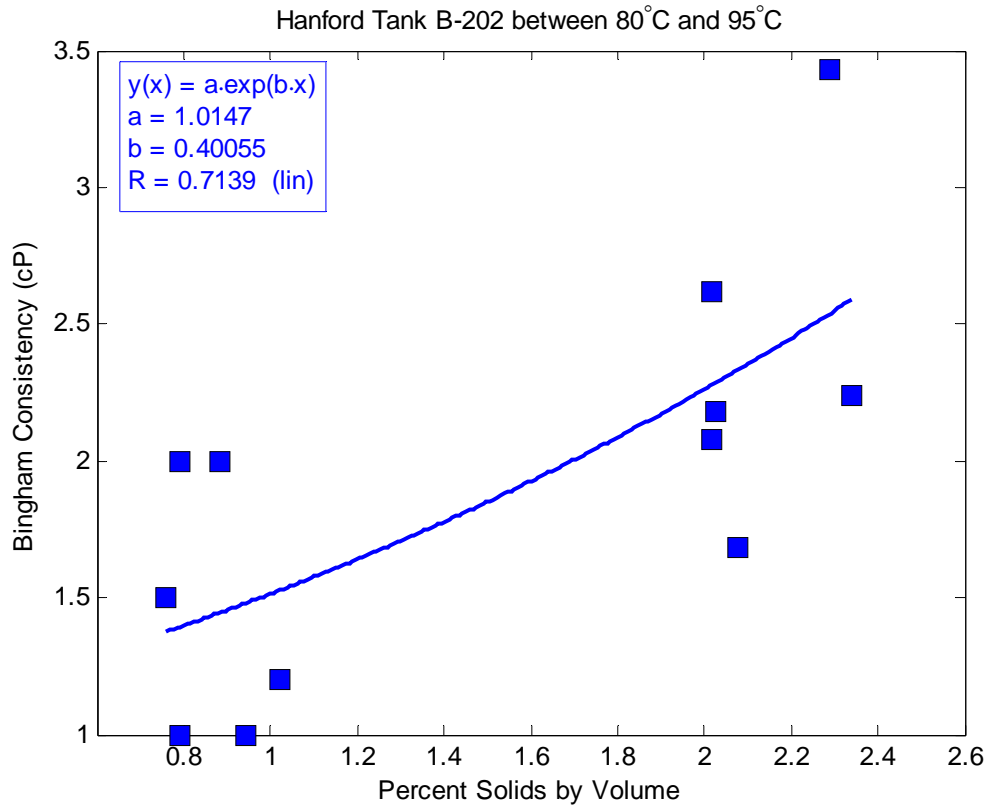


Hanford Tank B-202 between 20°C and 35°C

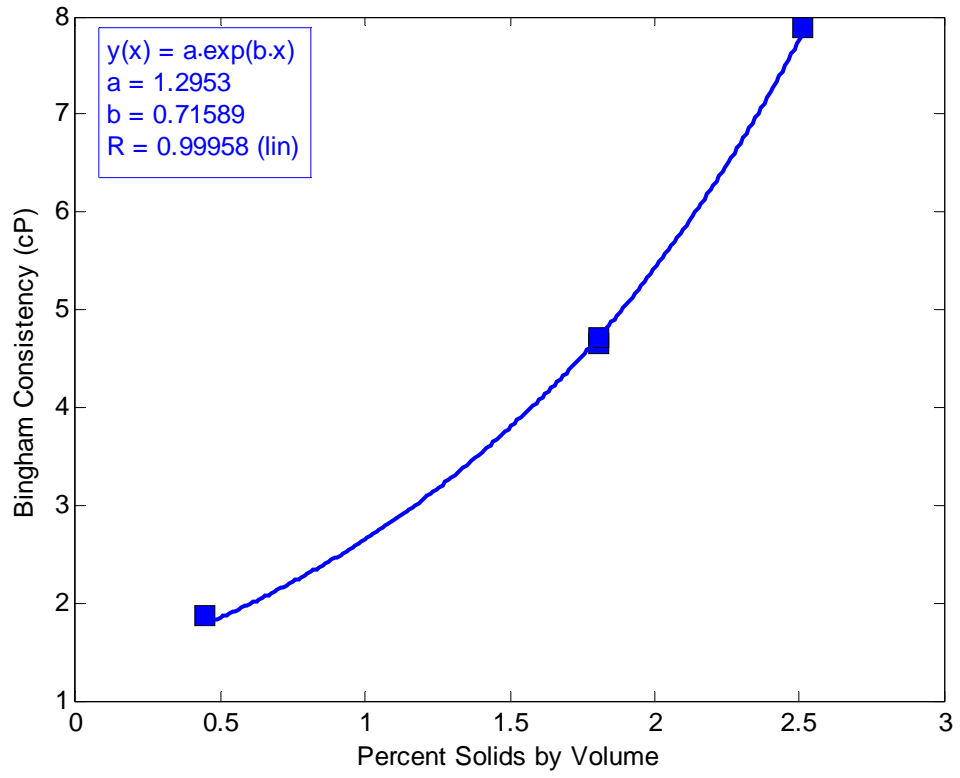


Hanford Tank B-202 between 20°C and 35°C

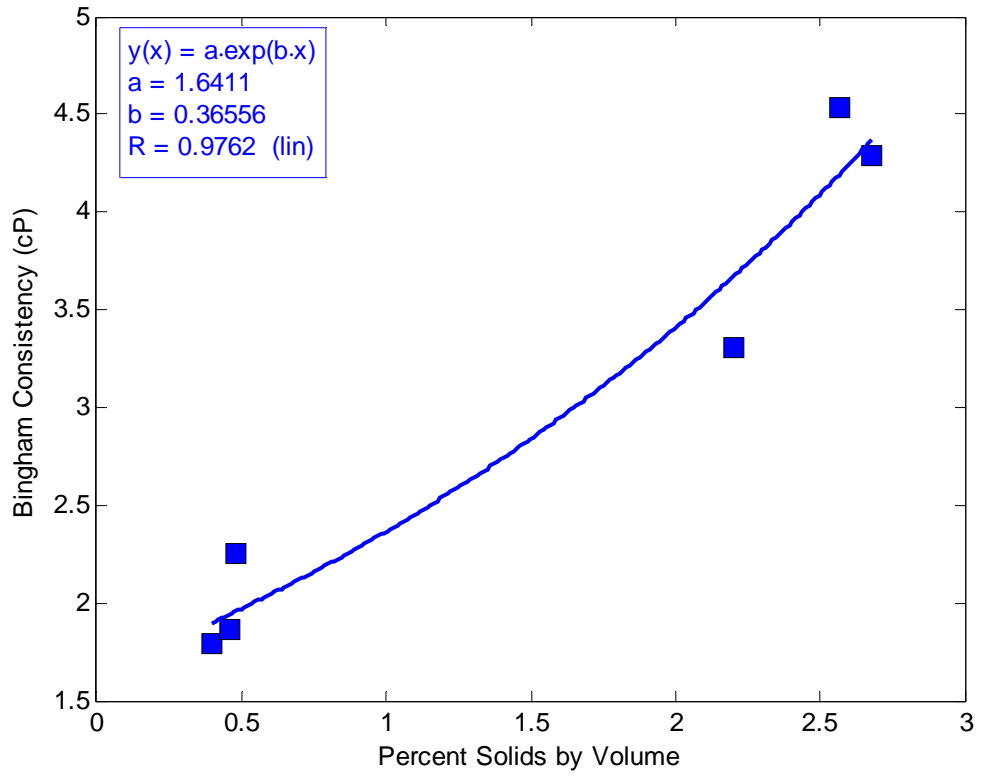




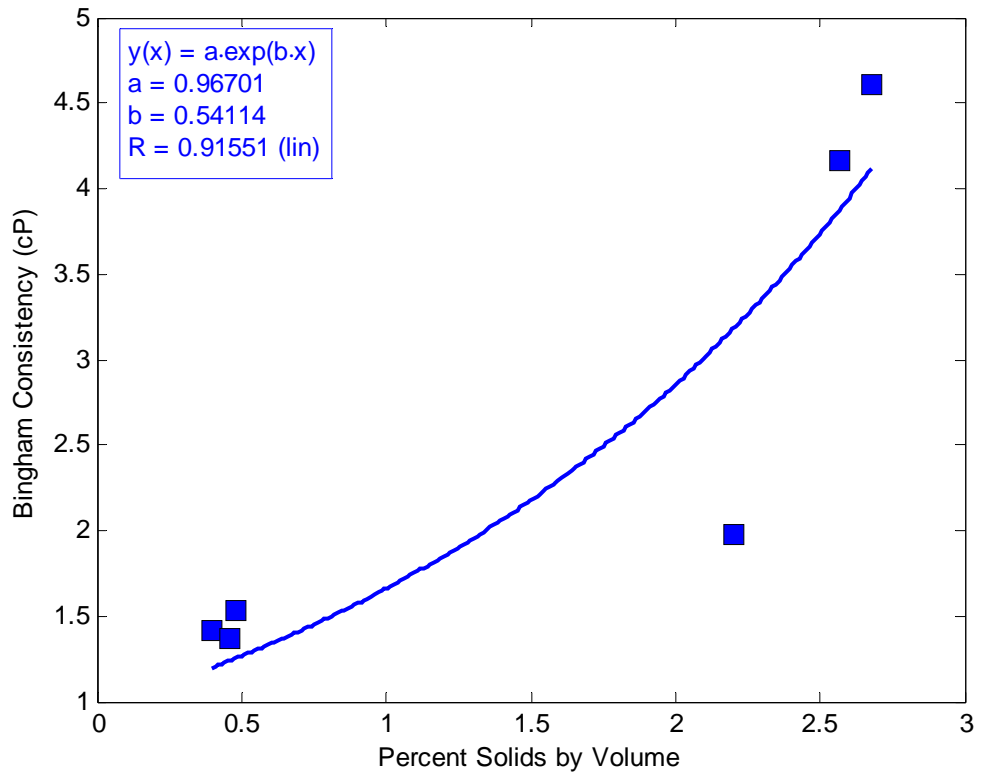
Hanford Tank B-203 between 20°C and 35°C



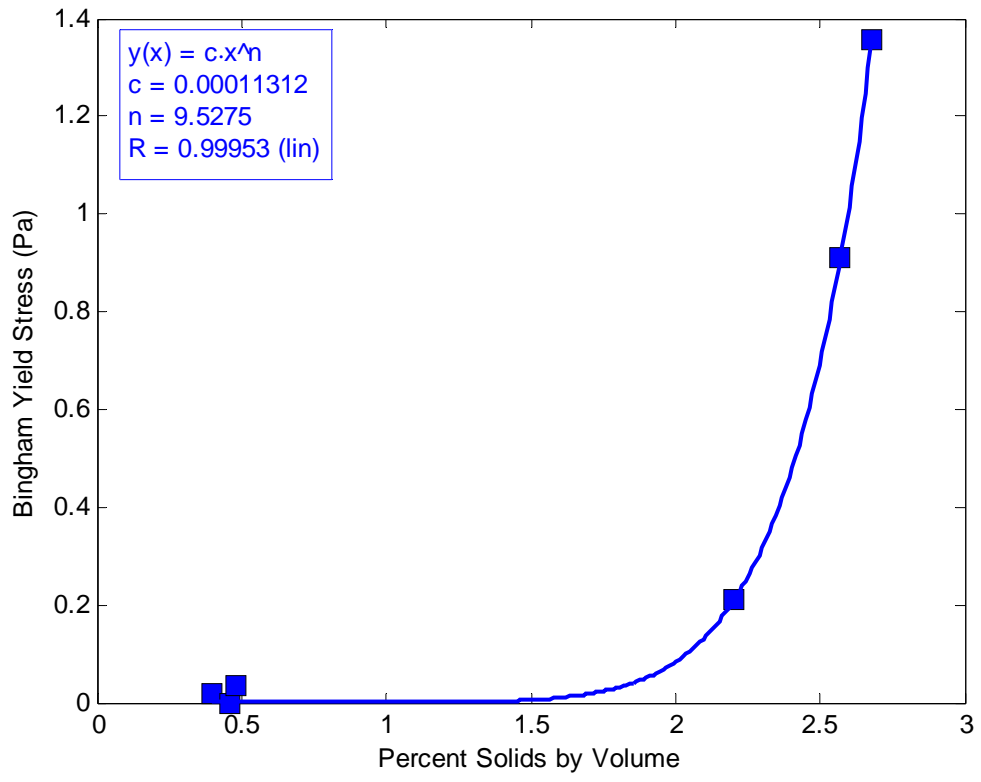
Hanford Tank BX-107 between 20°C and 35°C

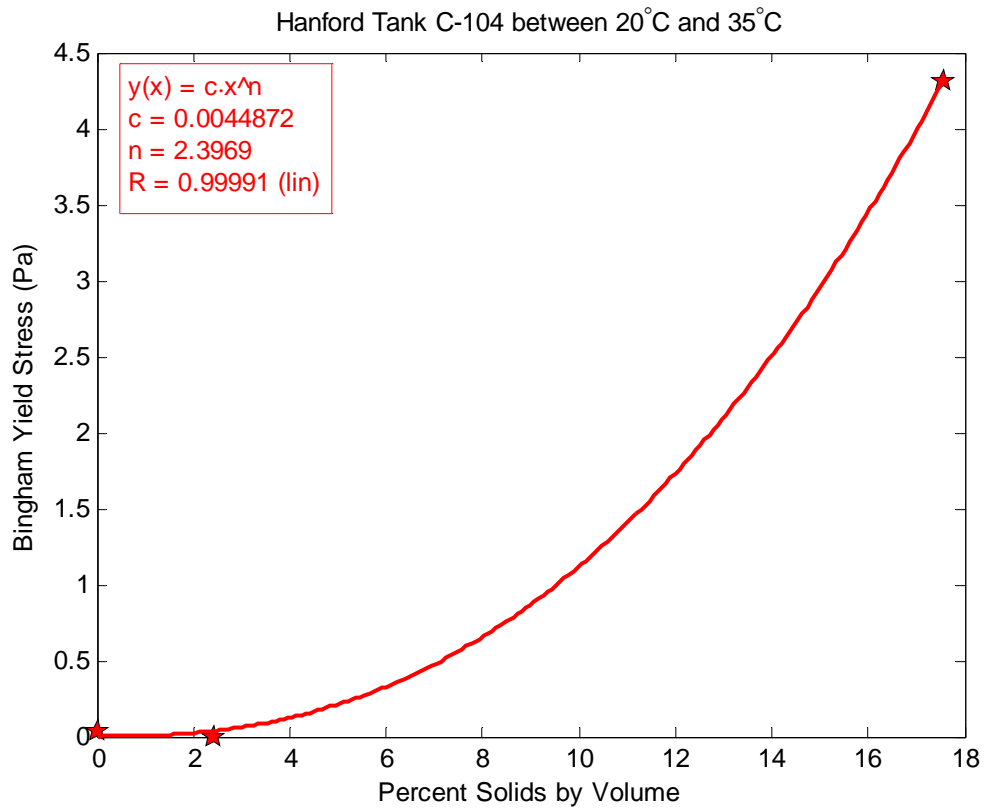
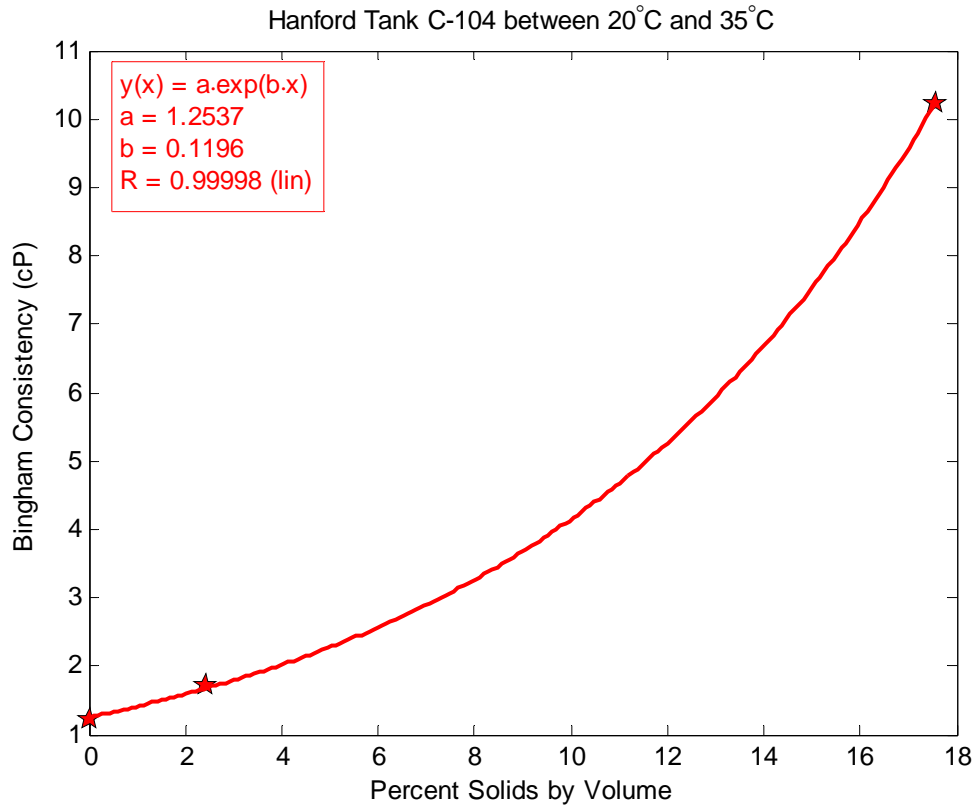


Hanford Tank BX-107 between 80°C and 95°C

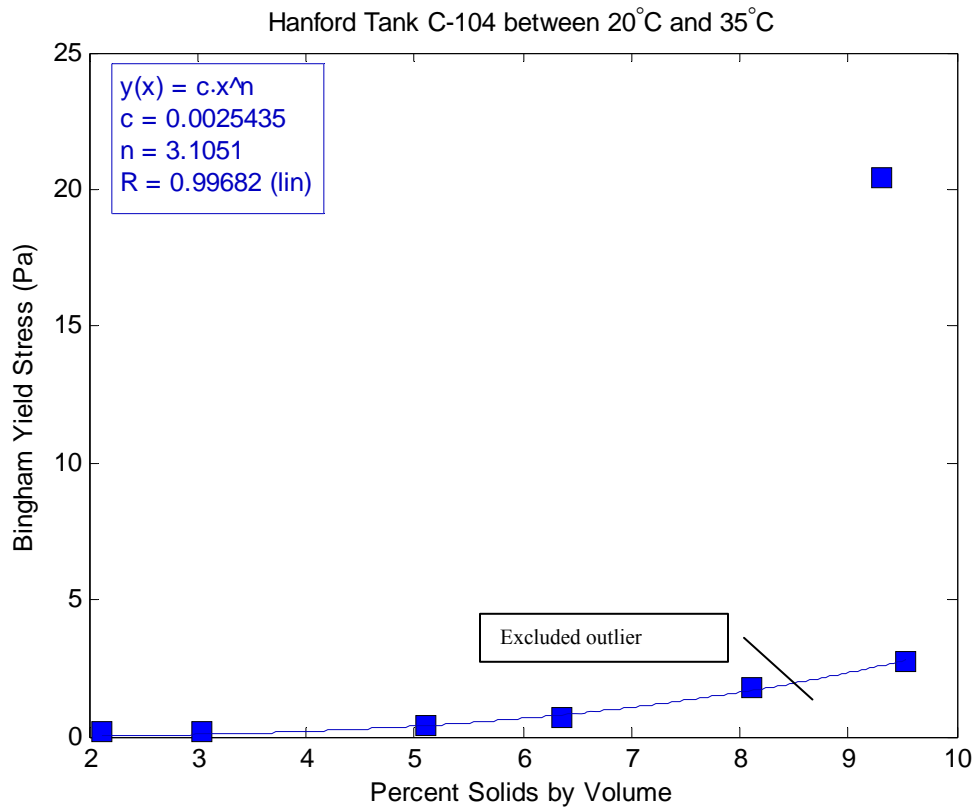
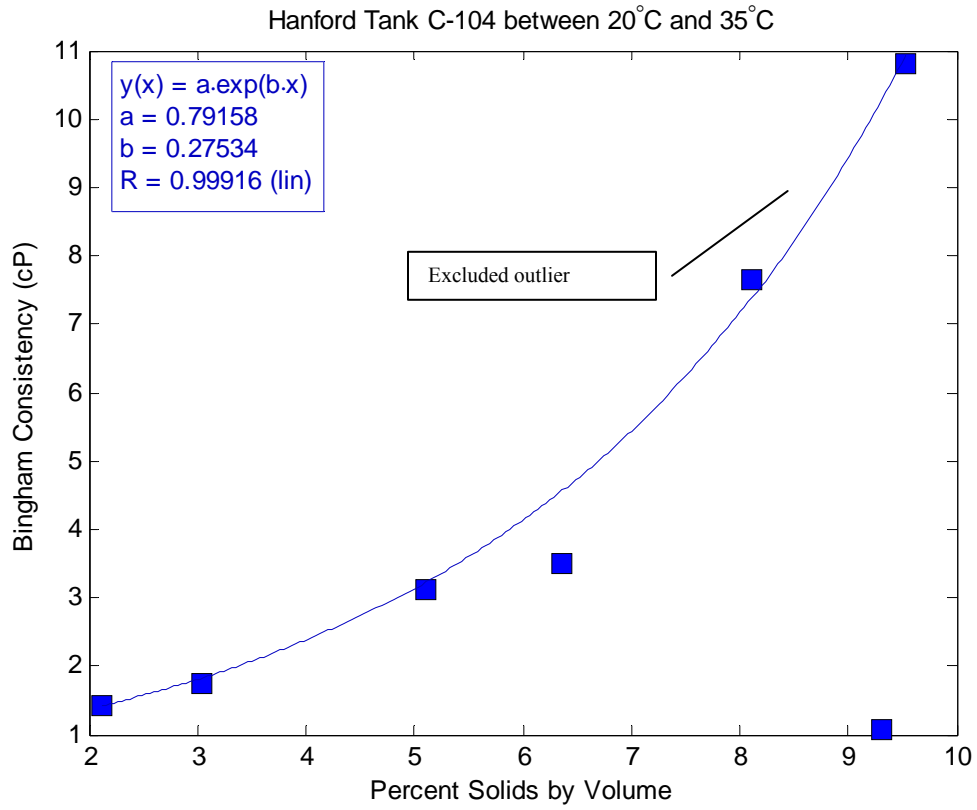


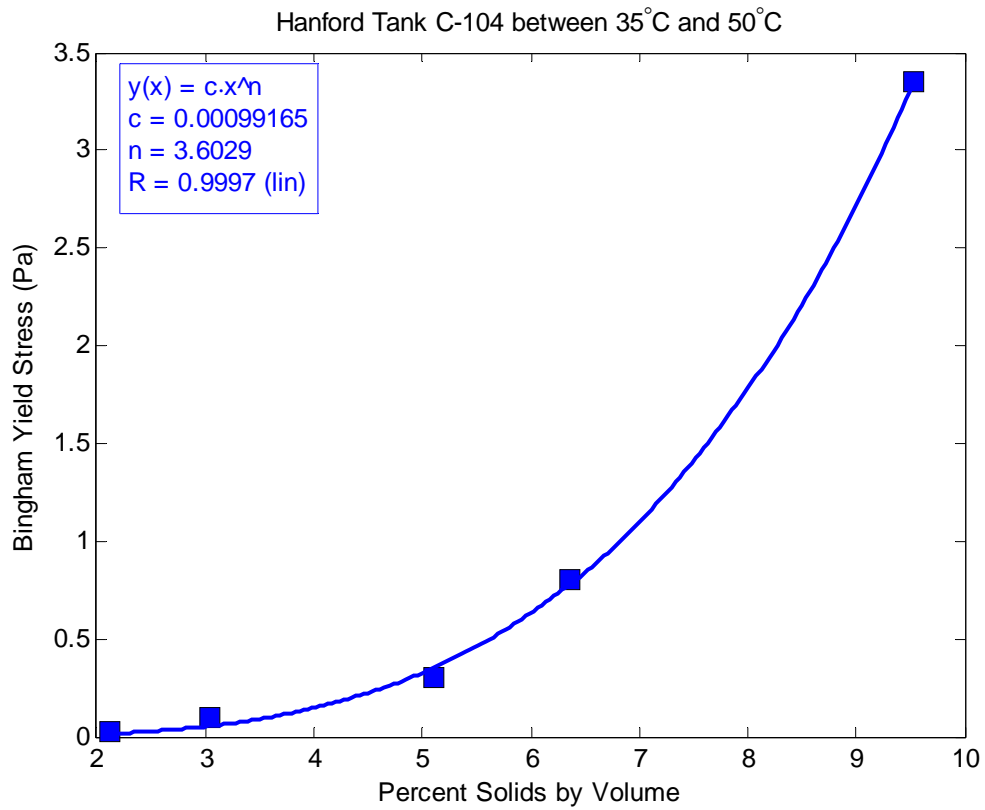
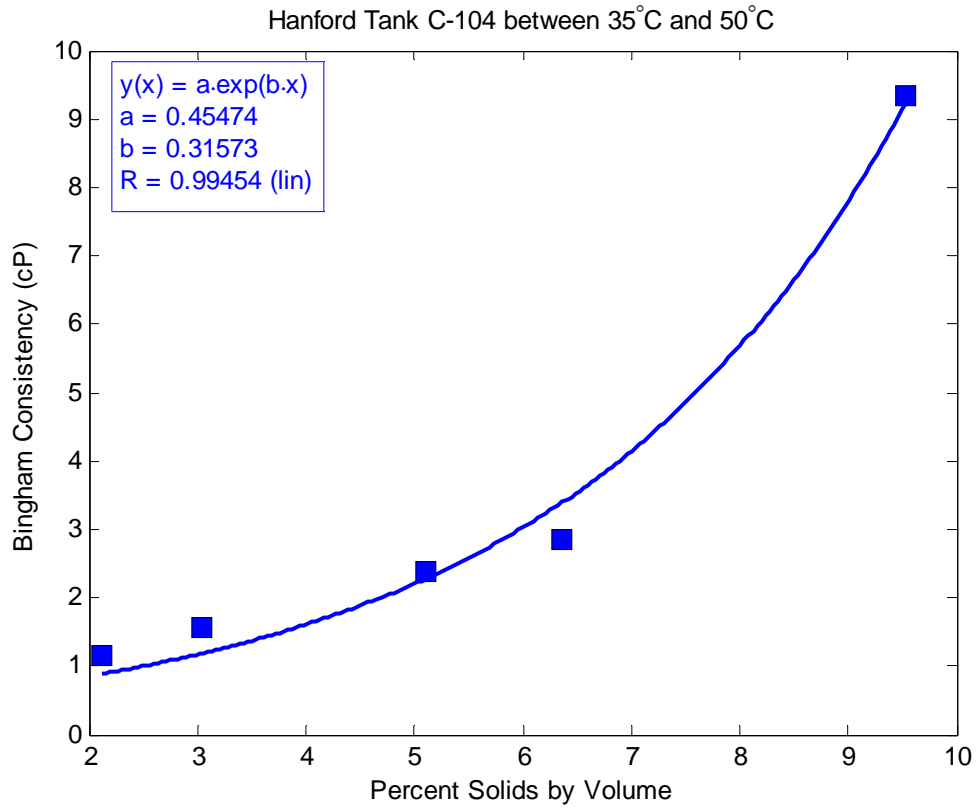
Hanford Tank BX-107 between 80°C and 95°C



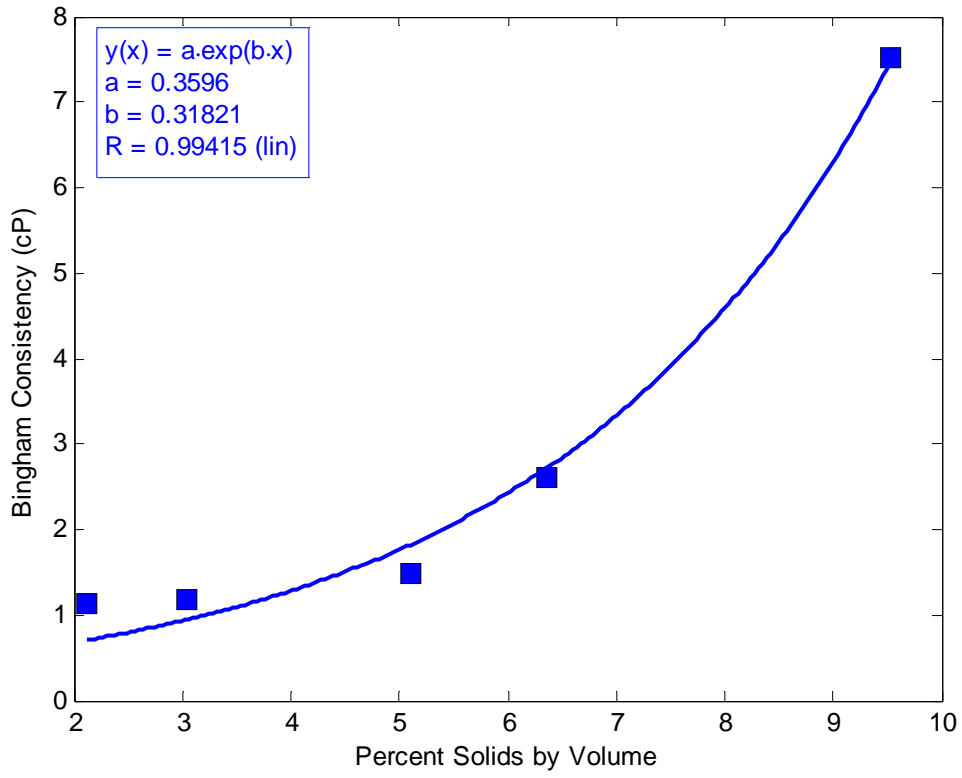




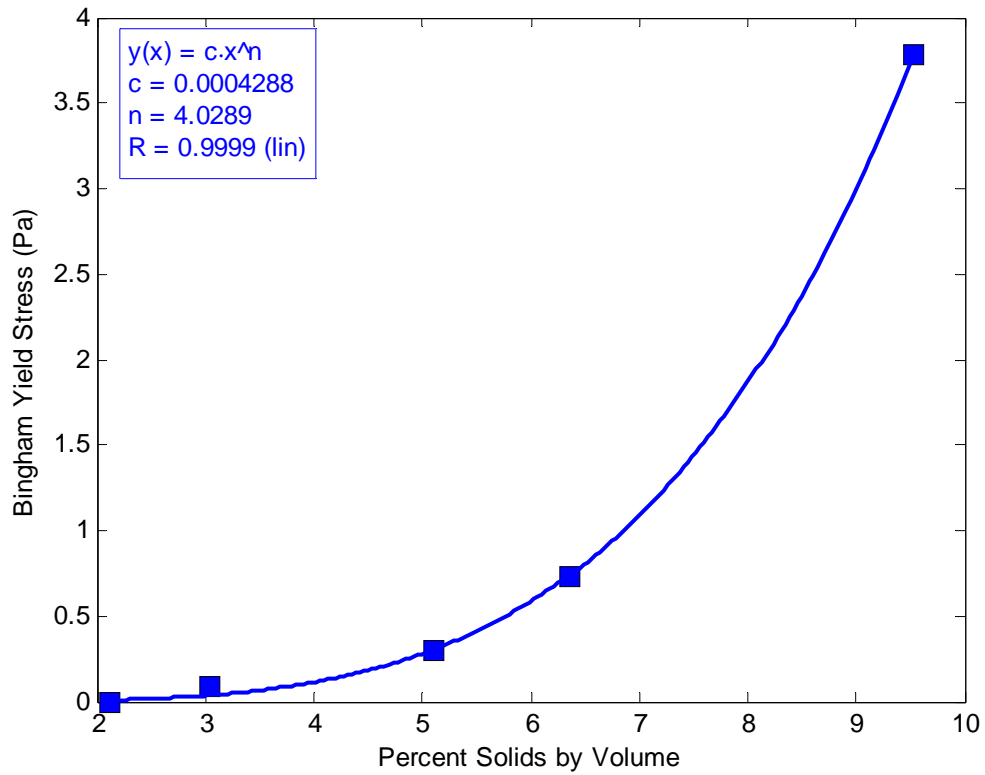




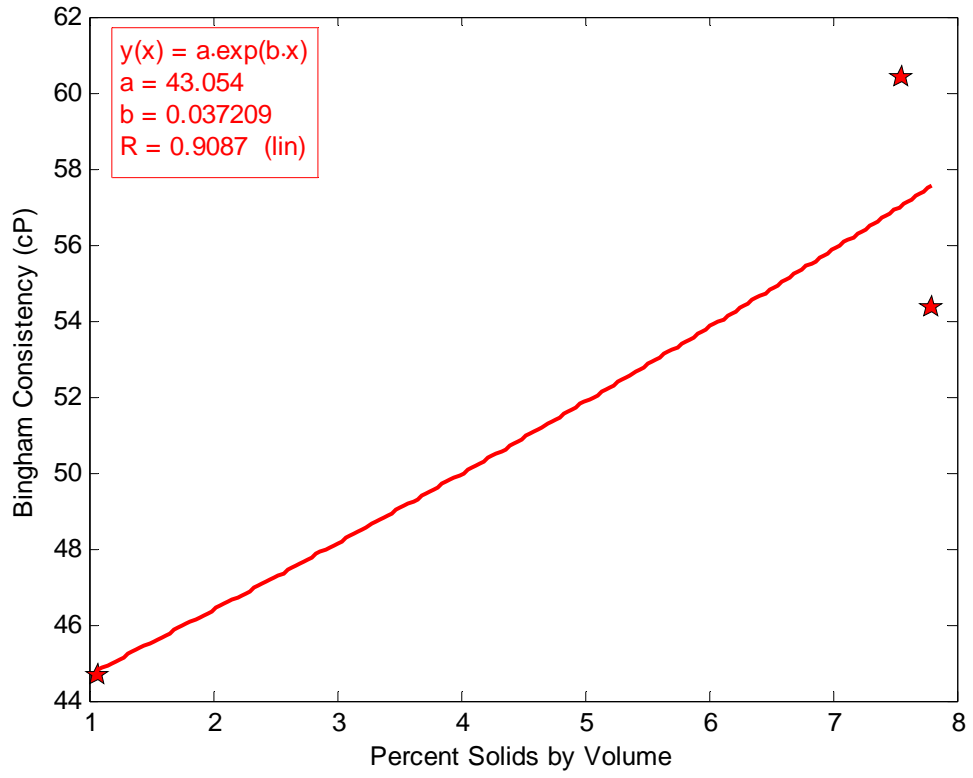
Hanford Tank C-104 between 50°C and 65°C



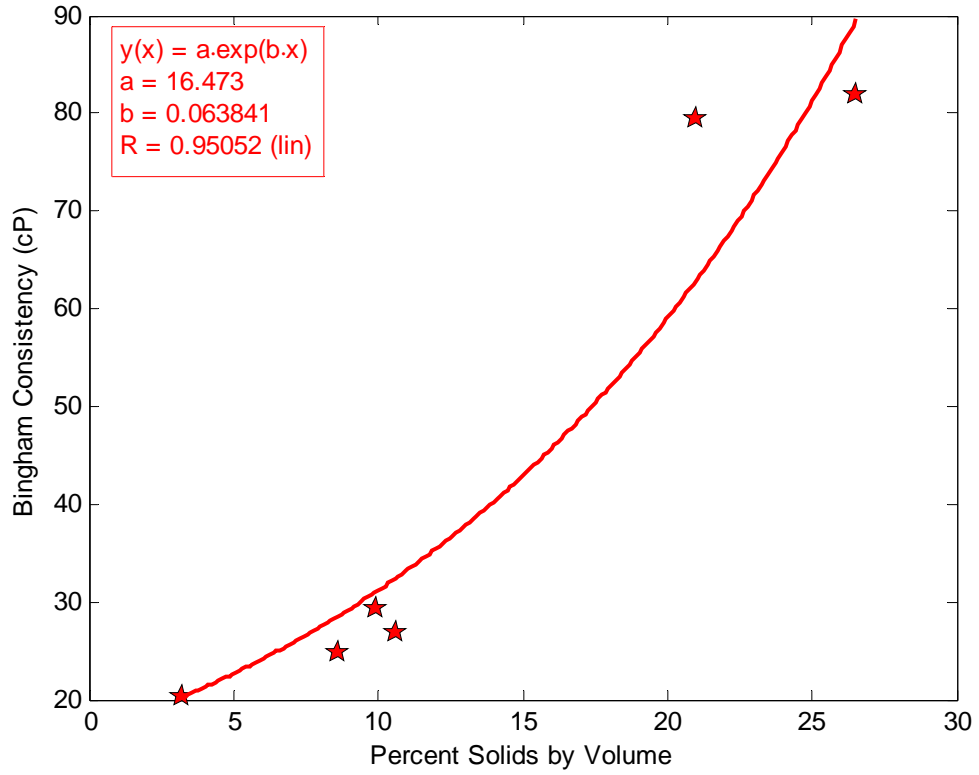
Hanford Tank C-104 between 50°C and 65°C



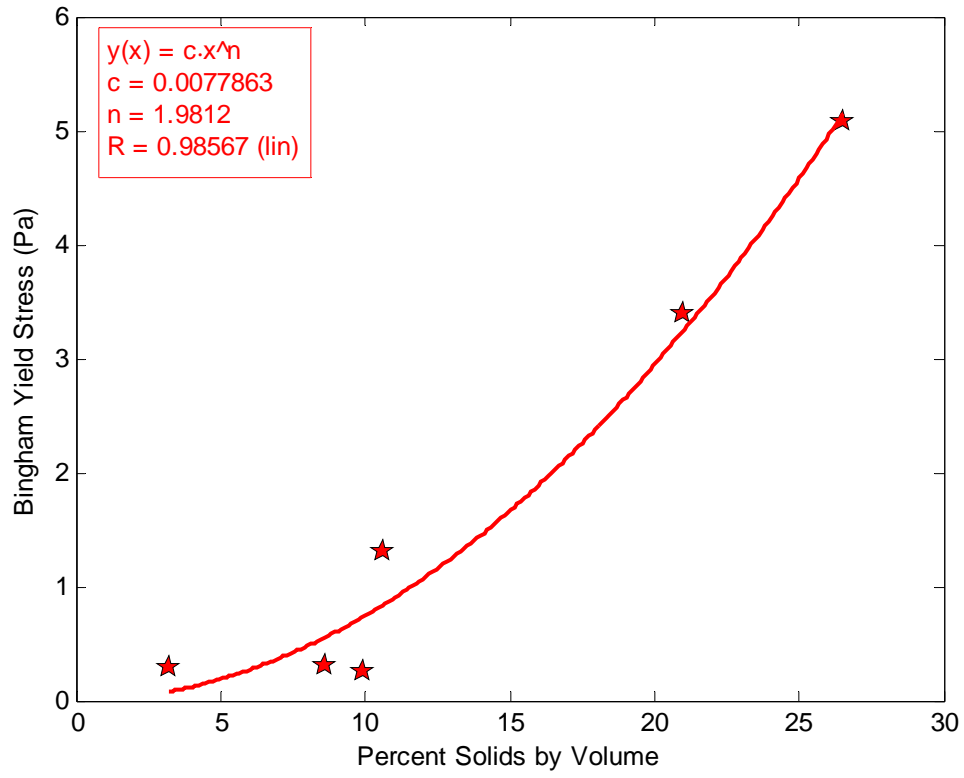
Hanford Tank SY-101 between 20°C and 35°C



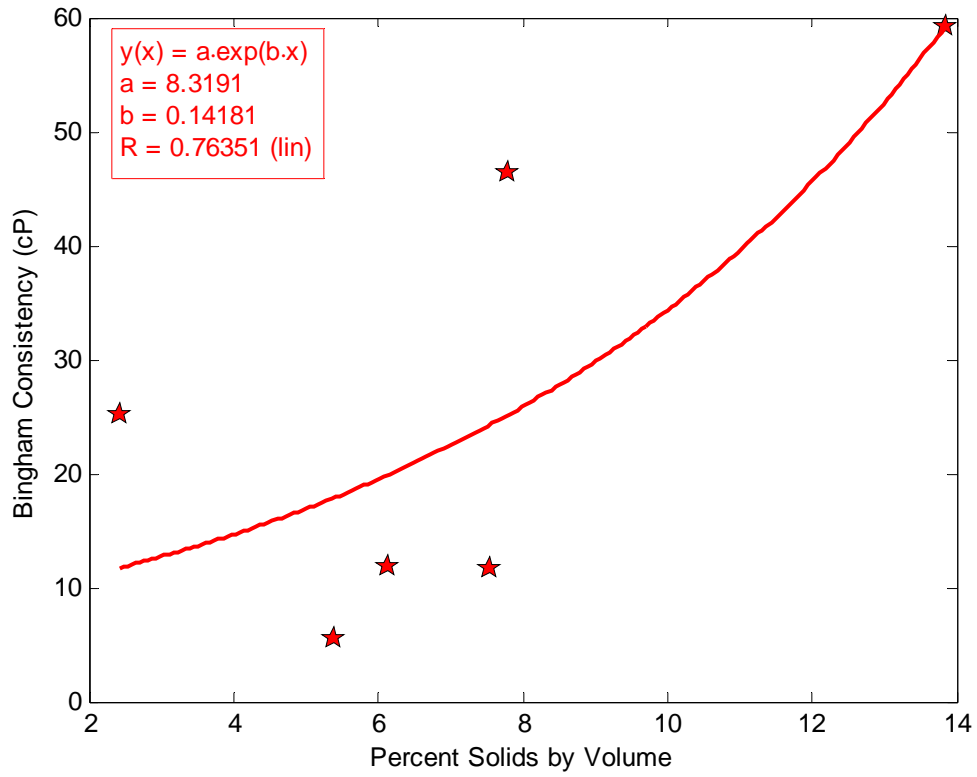
Hanford Tank SY-101 between 35°C and 50°C



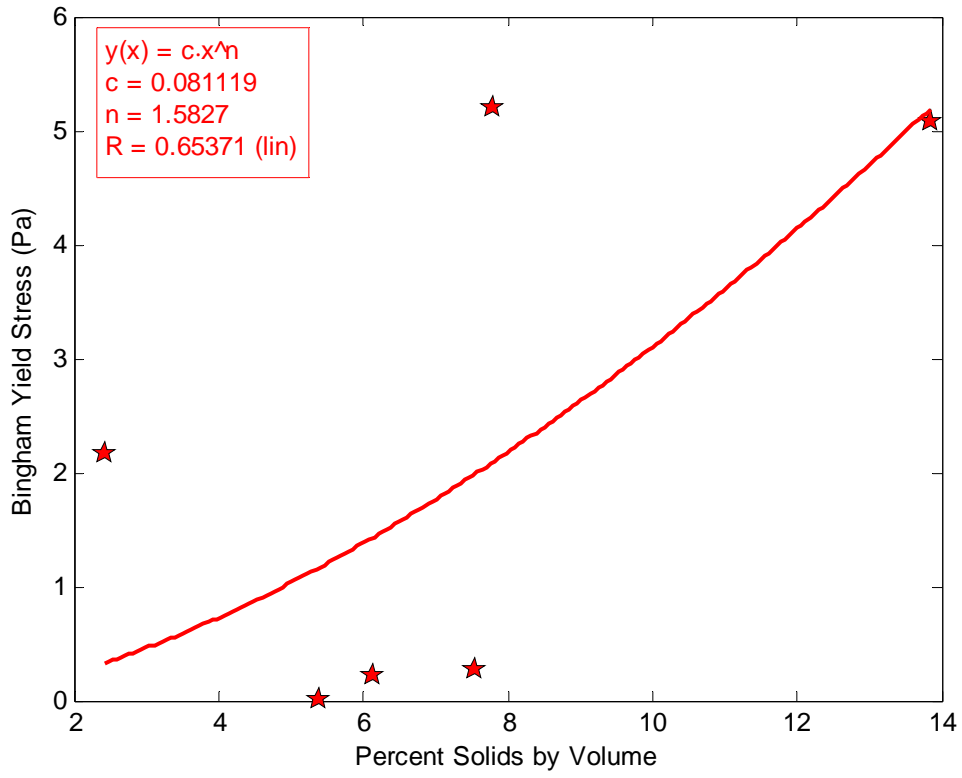
Hanford Tank SY-101 between 35°C and 50°C



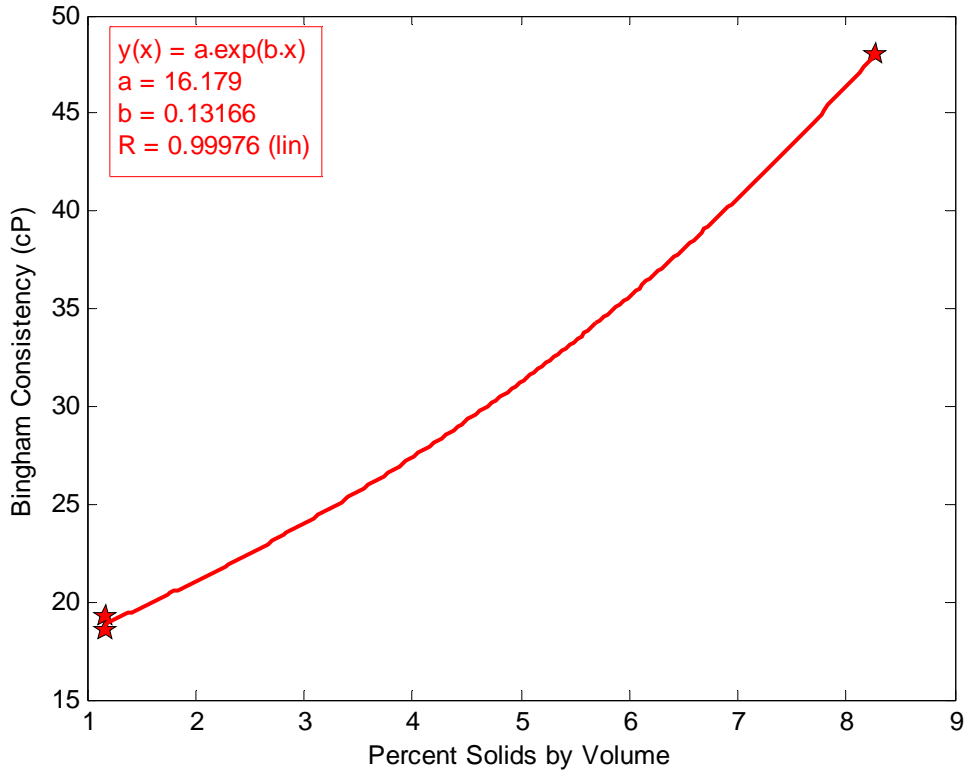
Hanford Tank SY-101 between 65°C and 80°C

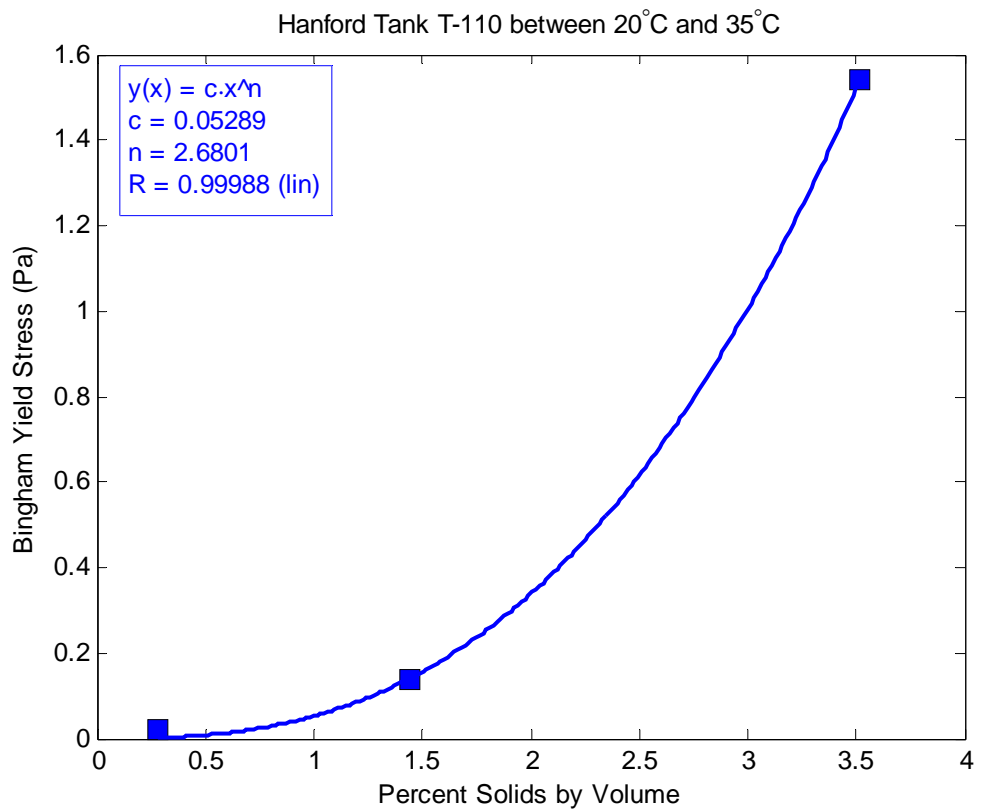
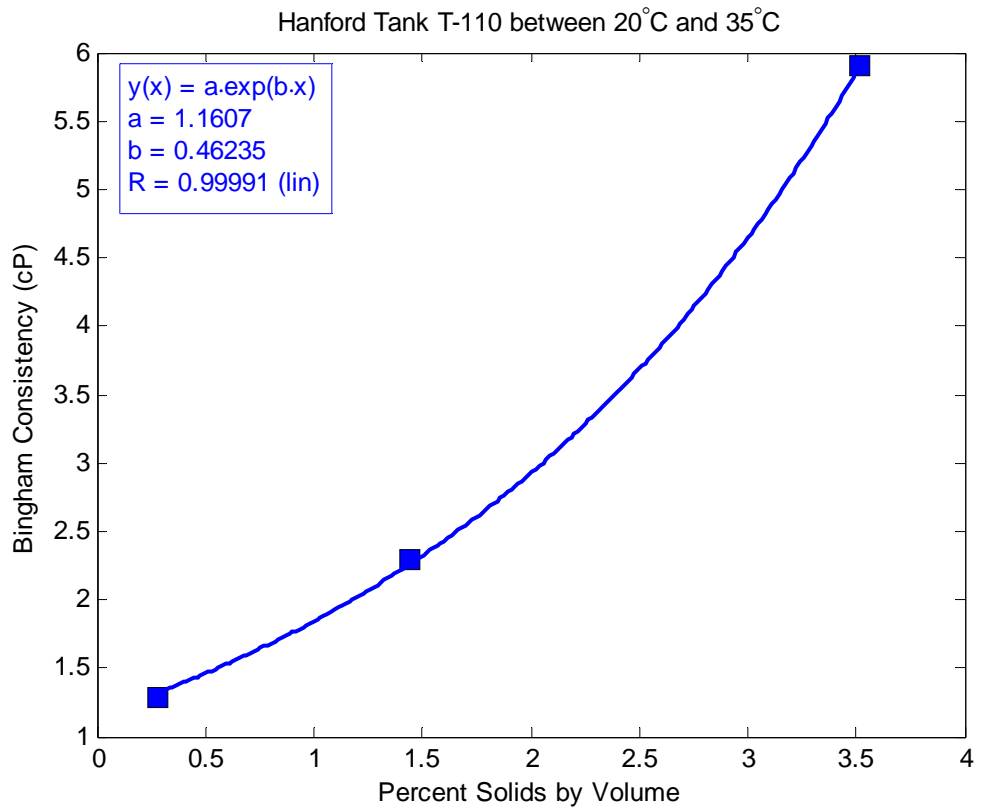


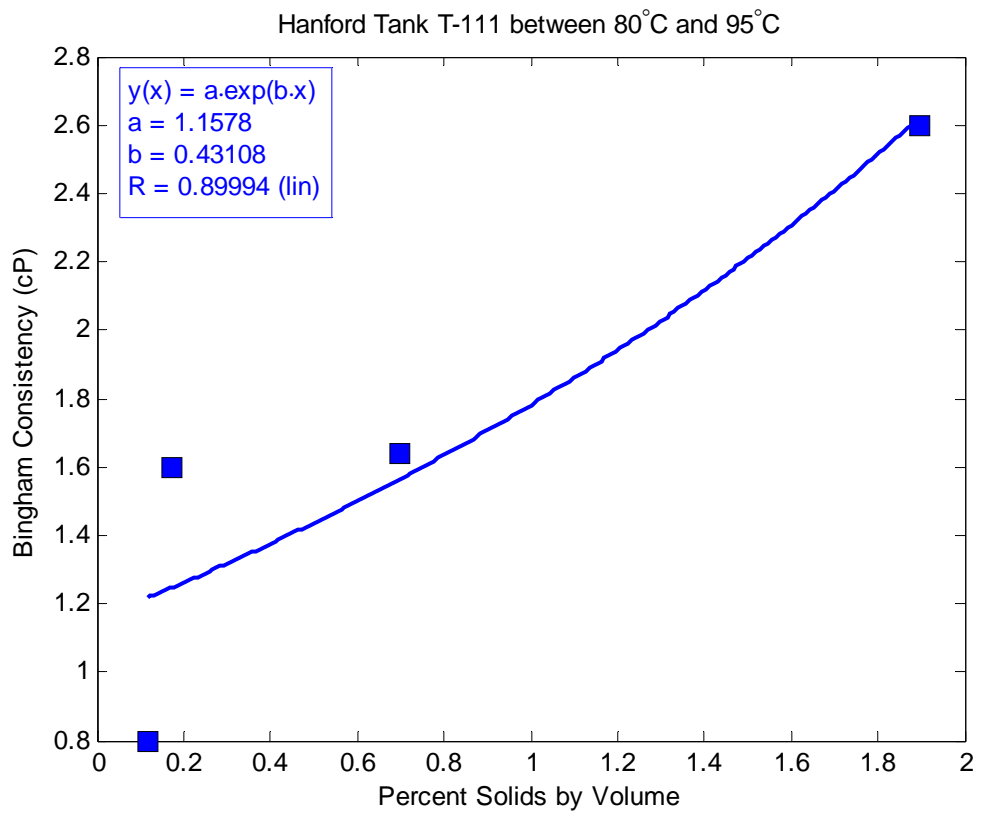
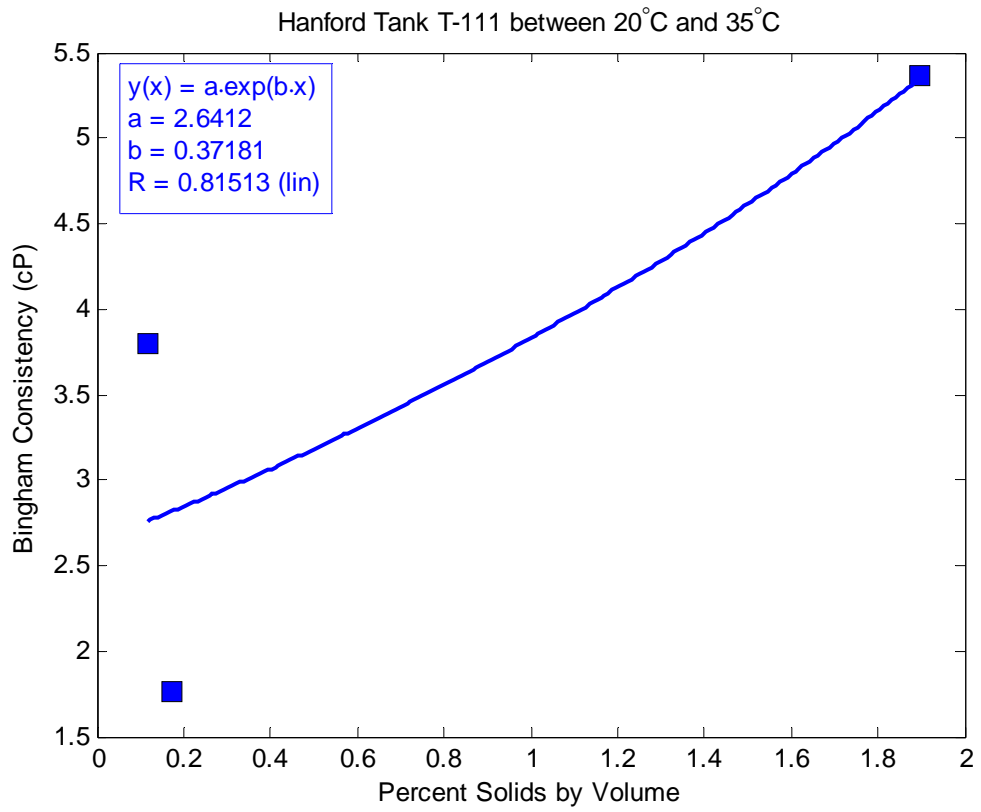
Hanford Tank SY-101 between 65°C and 80°C



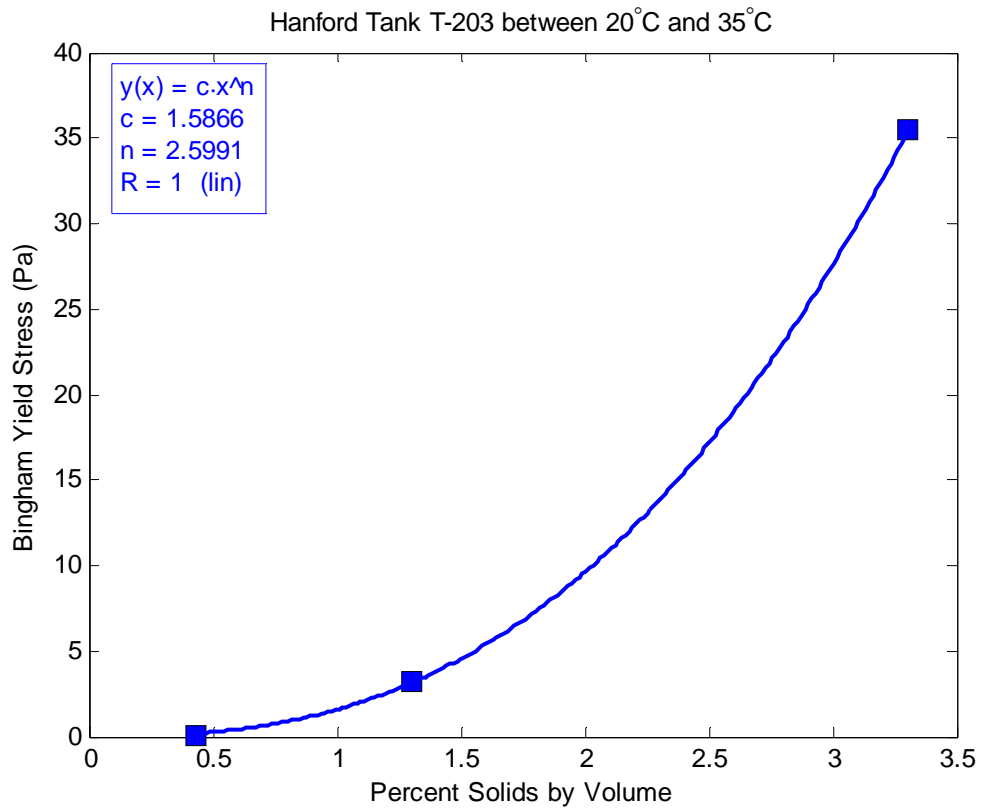
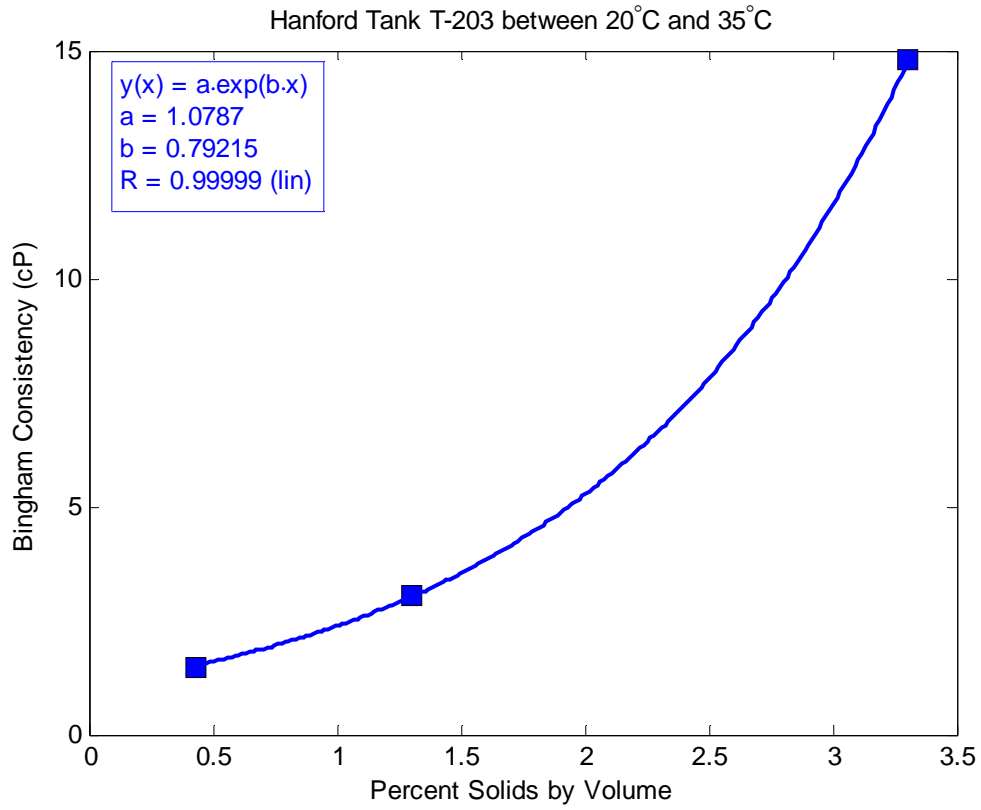
Hanford Tank SY-101 between 80°C and 95°C









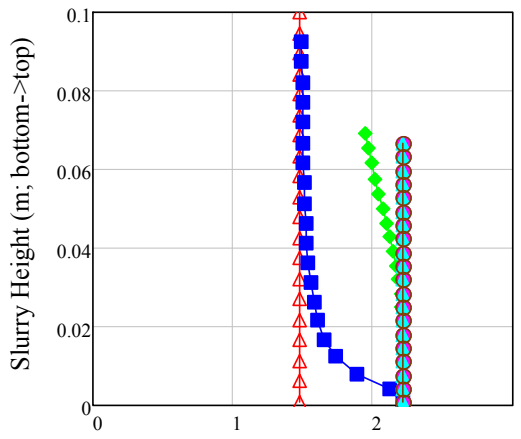


## **Appendix D**

### **Sedimentation Layer Properties as Sludge Settles Under Different Starting Heights**

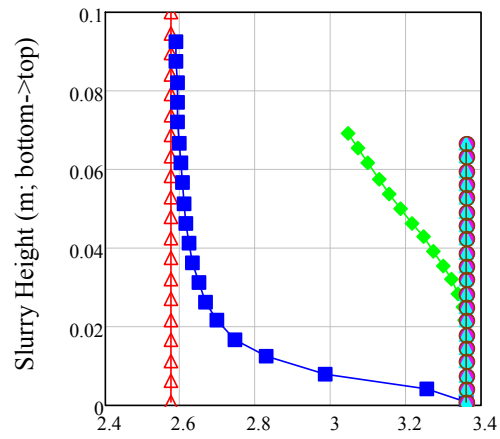
# Appendix D – Sedimentation Layer Properties as Sludge Settles Under Different Starting Heights

Predicted sludge properties from Hanford Tank B-202 with water dilution at a starting slurry height of 0.1 m with 33% volume excess supernatant from fully settled configuration; rheological properties taken at a temperature range of 20°–35°C.



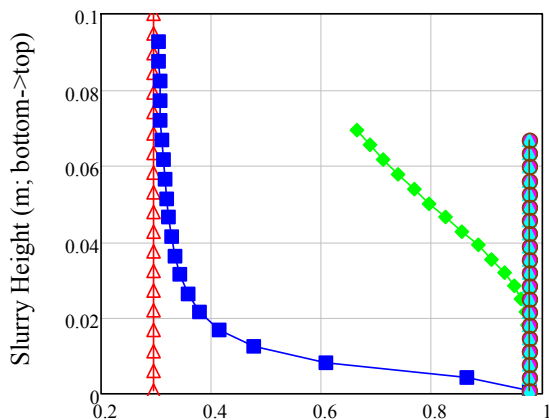
Solids Concentration (Volume Percent)

- △△ 0 hr
- 1 hr
- ◆ 10 hr
- 100 hr
- ▲ 200 hr
- 1000 hr



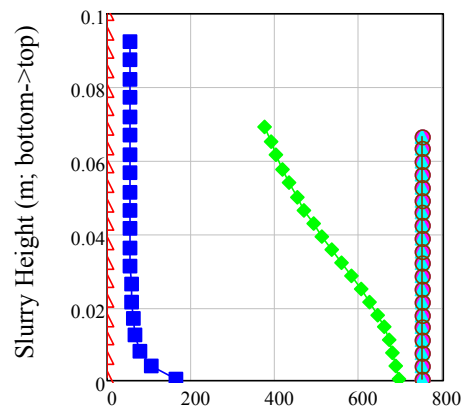
Bingham Consistency (cP)

- △△ 0 hr
- 1 hr
- ◆ 10 hr
- 100 hr
- ▲ 200 hr
- 1000 hr



Bingham Yield Stress (Pa)

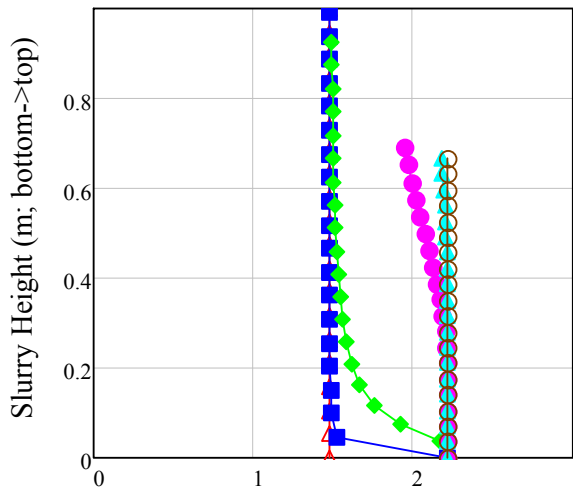
- △△ 0 hr
- 1 hr
- ◆ 10 hr
- 100 hr
- ▲ 200 hr
- 1000 hr



Shear Strength (Pa)

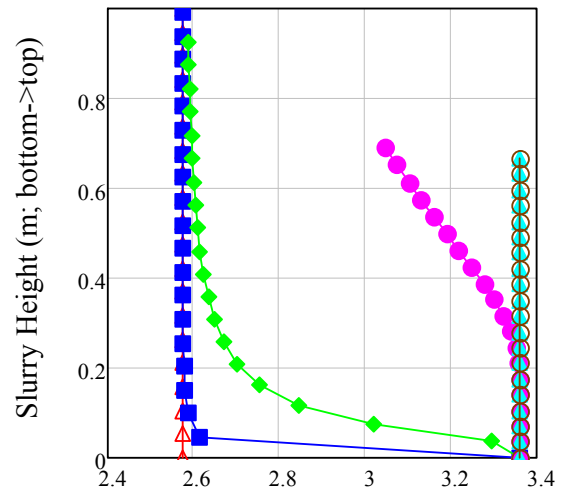
- △△ 0 hr
- 1 hr
- ◆ 10 hr
- 100 hr
- ▲ 200 hr
- 1000 hr

Predicted sludge properties from Hanford Tank B-202 with water dilution at a starting slurry height of 1 m with 33% volume excess supernatant from fully settled configuration; rheological properties taken at a temperature range of 20°–35°C.



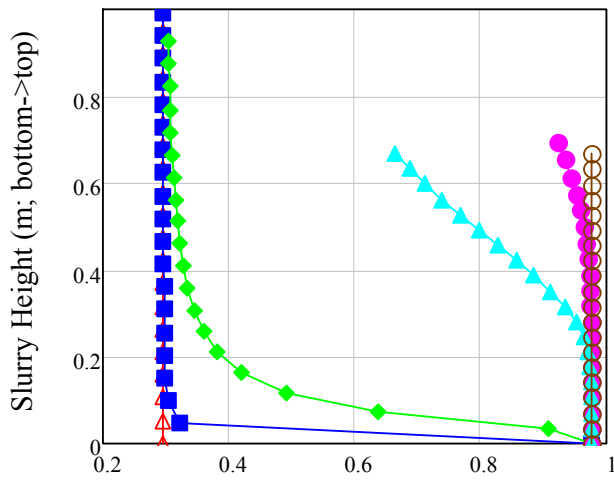
Solids Concentration (Volume Percent)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



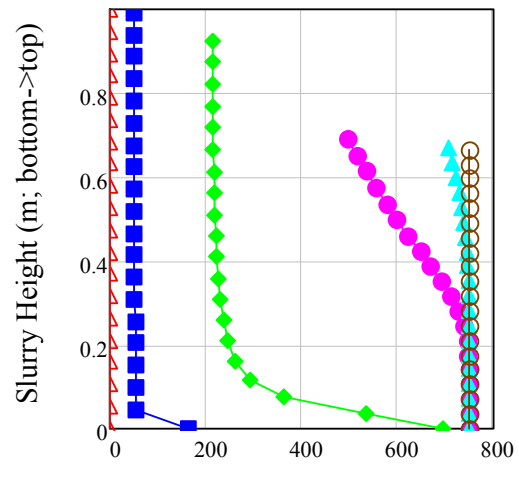
Bingham Consistency (cP)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



Bingham Yield Stress (Pa)

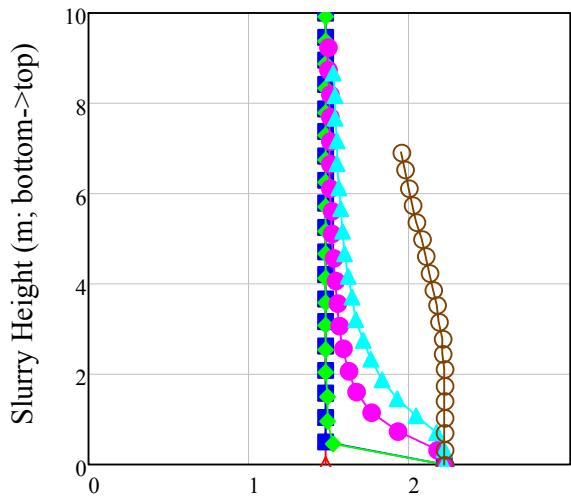
- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



Shear Strength(Pa)

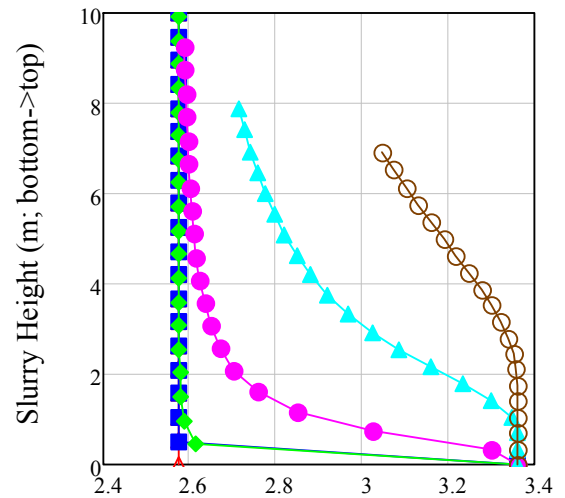
- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr

Predicted sludge properties from Hanford Tank B-202 with water dilution at a starting slurry height of 10 m with 33% volume excess supernatant from fully settled configuration; rheological properties taken at a temperature range of 20°–35°C.



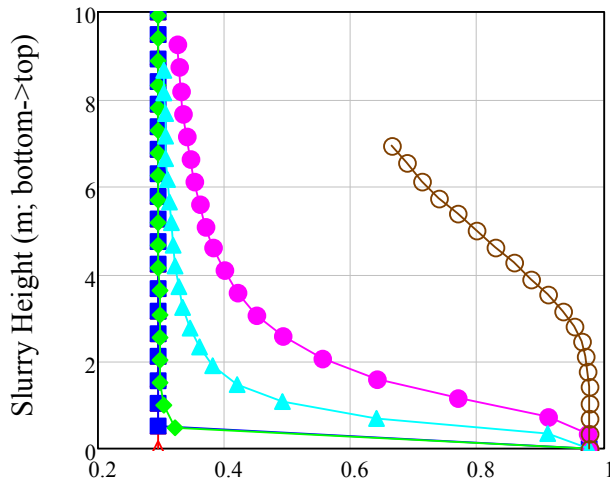
Solids Concentration (Volume Percent)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- ⊖⊖ 1000 hr



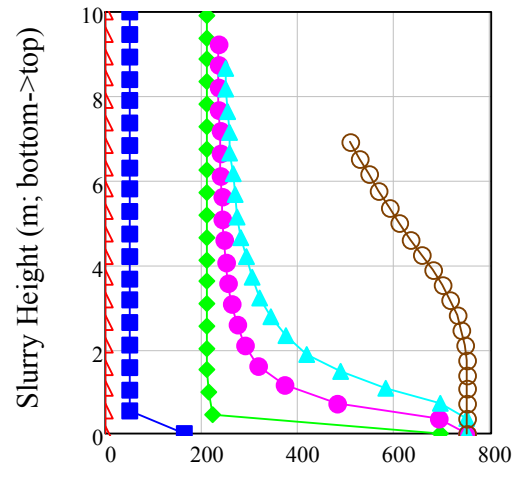
Bingham Consistency (cP)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- ⊖⊖ 1000 hr



Bingham Yield Stress (Pa)

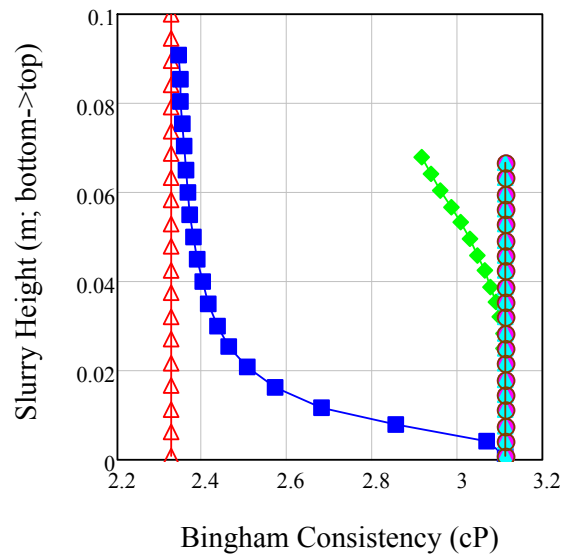
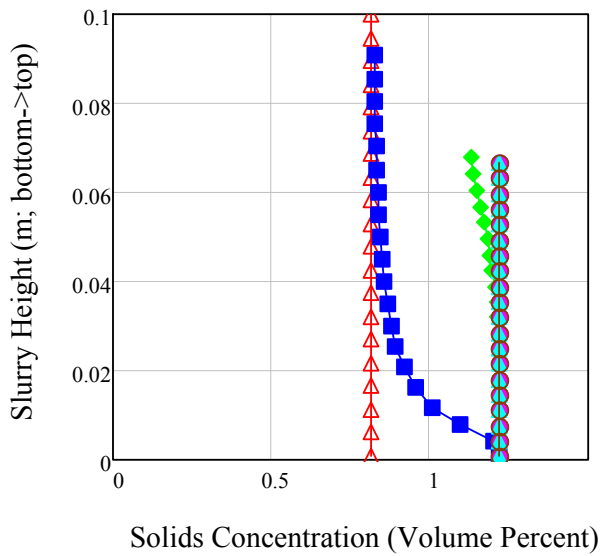
- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- ⊖⊖ 1000 hr



Shear Strength(Pa)

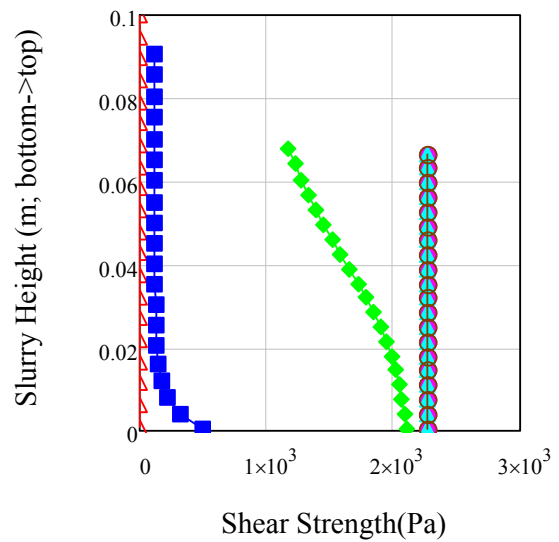
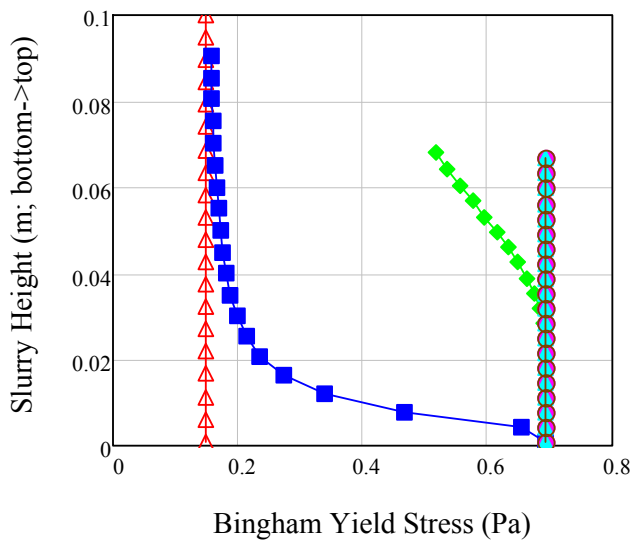
- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- ⊖⊖ 1000 hr

Predicted sludge properties from Hanford Tank B-203 with water dilution at a starting slurry height of 0.1 m with 33% volume excess supernatant from fully settled configuration; rheological properties taken at a temperature range of 20°–35°C.



- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr

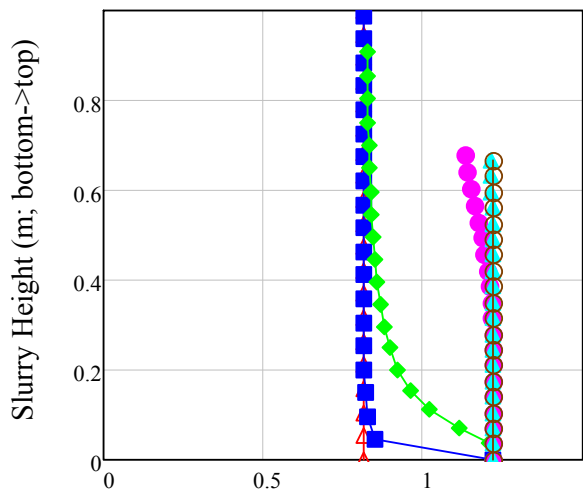
- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr

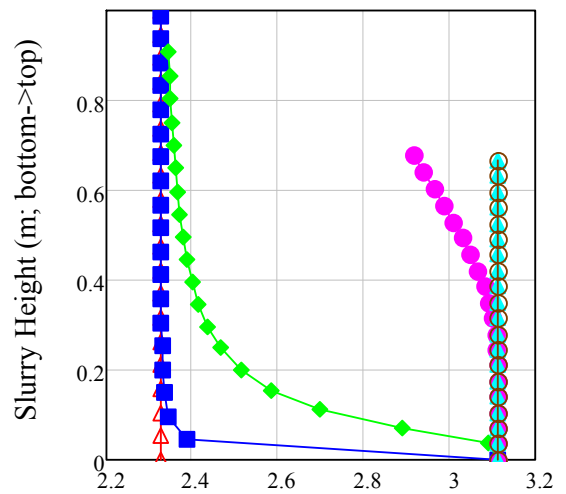
- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr

Predicted sludge properties from Hanford Tank B-203 with water dilution at a starting slurry height of 1 m with 33% volume excess supernatant from fully settled configuration; rheological properties taken at a temperature range of 20°–35°C.



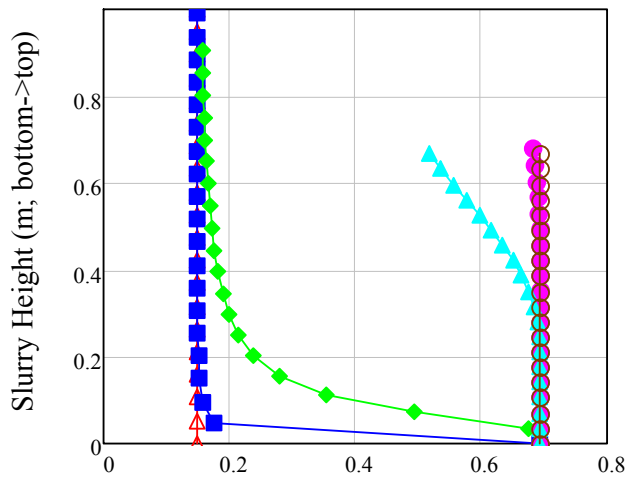
Solids Concentration (Volume Percent)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



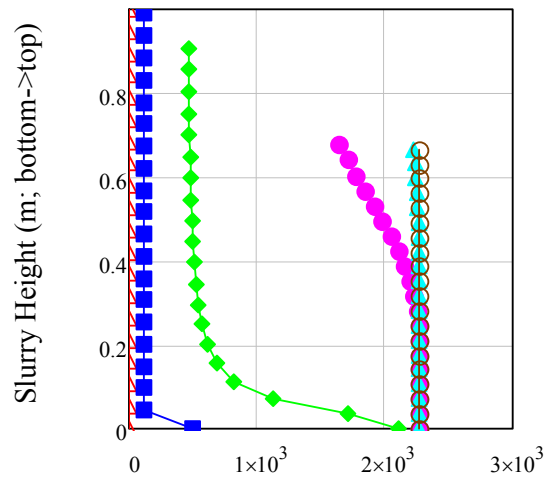
Bingham Consistency (cP)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



Bingham Yield Stress (Pa)

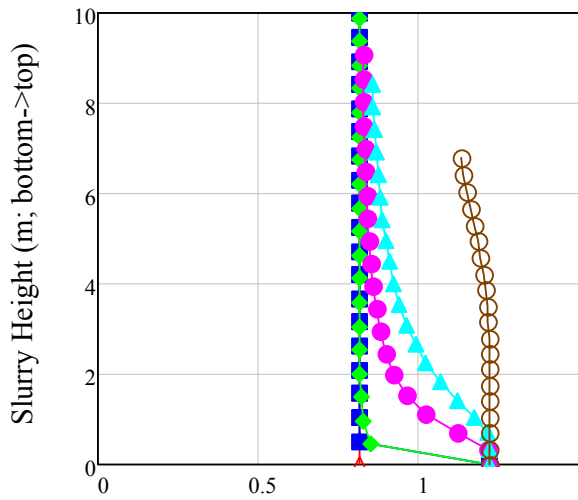
- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



Shear Strength (Pa)

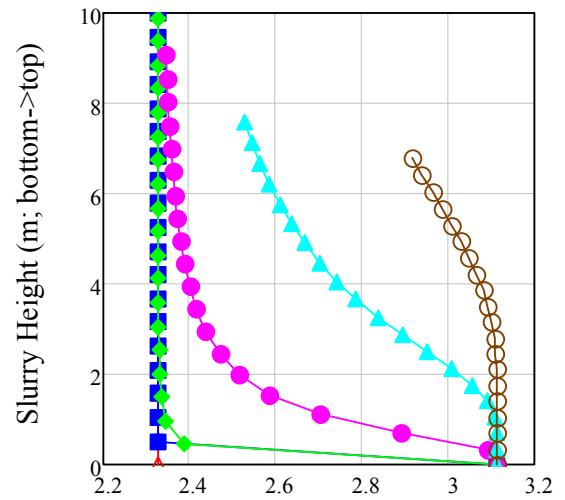
- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr

Predicted sludge properties from Hanford Tank B-203 with water dilution at a starting slurry height of 10 m with 33% volume excess supernatant from fully settled configuration; rheological properties taken at a temperature range of 20°–35°C.



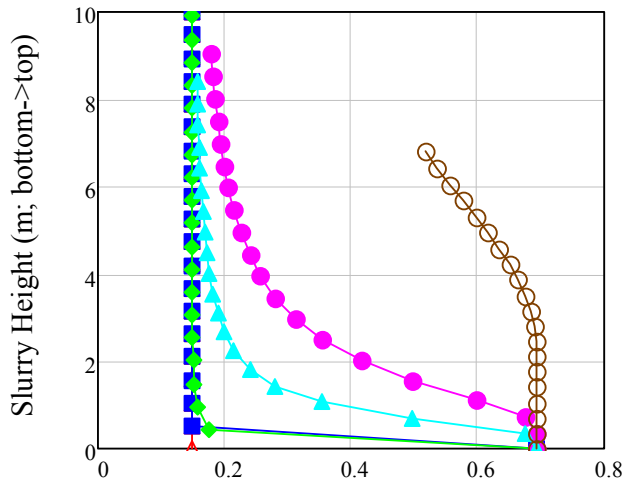
Solids Concentration (Volume Percent)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



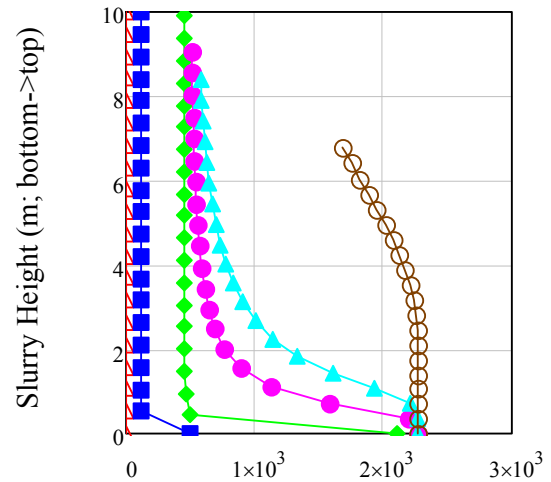
Bingham Consistency (cP)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



Bingham Yield Stress (Pa)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr

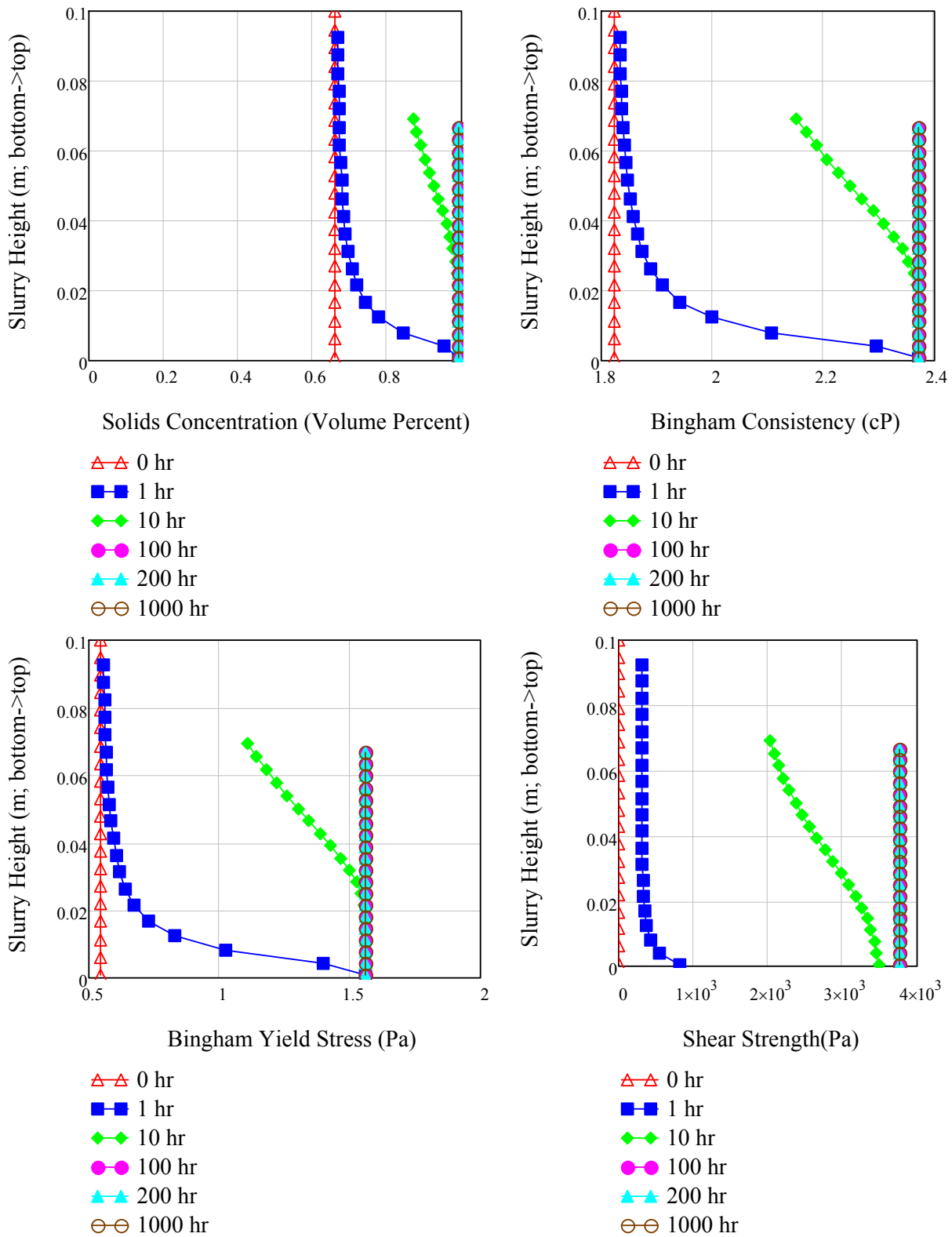


Shear Strength(Pa)

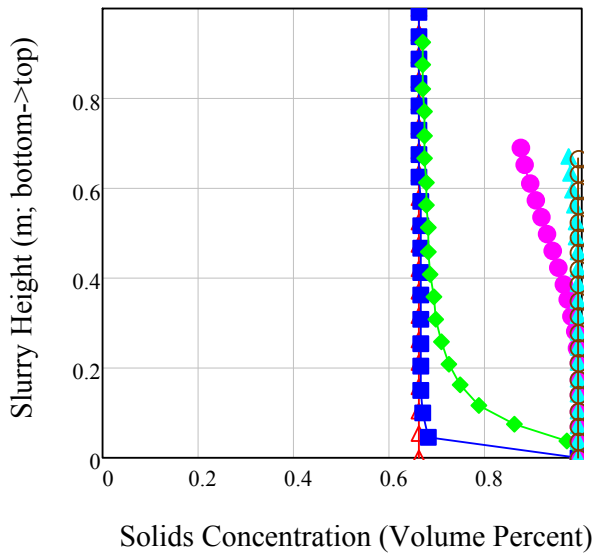
- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



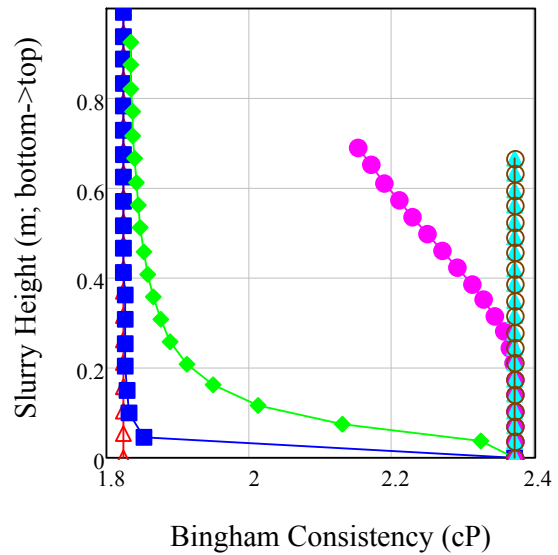
Predicted sludge properties from Hanford Tank T-203 with water dilution at a starting slurry height of 0.1 m with 33% volume excess supernatant from fully settled configuration; rheological properties taken at a temperature range of 20°–5°C.



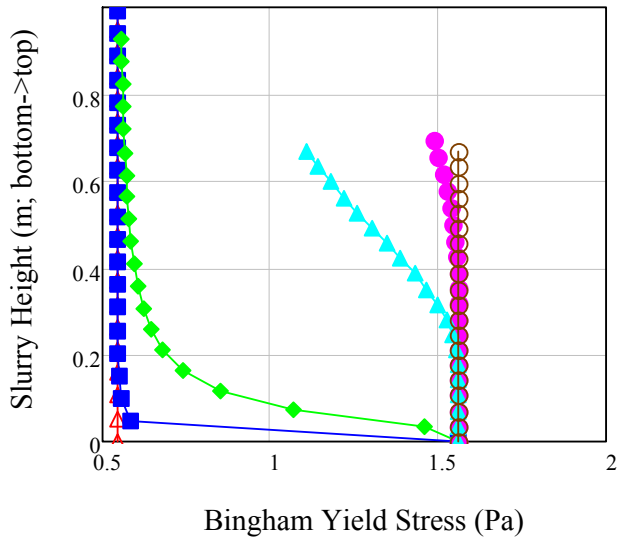
Predicted sludge properties from Hanford Tank T-203 with water dilution at a starting slurry height of 1 m with 33% volume excess supernatant from fully settled configuration; rheological properties taken at a temperature range of 20°–35°C.



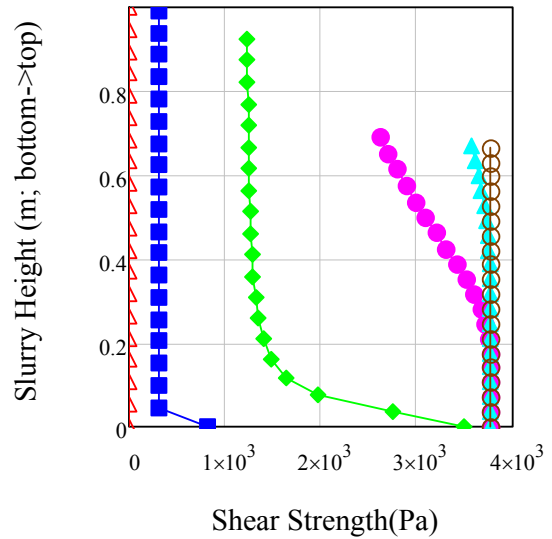
- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- ⊖⊖ 1000 hr



- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- ⊖⊖ 1000 hr

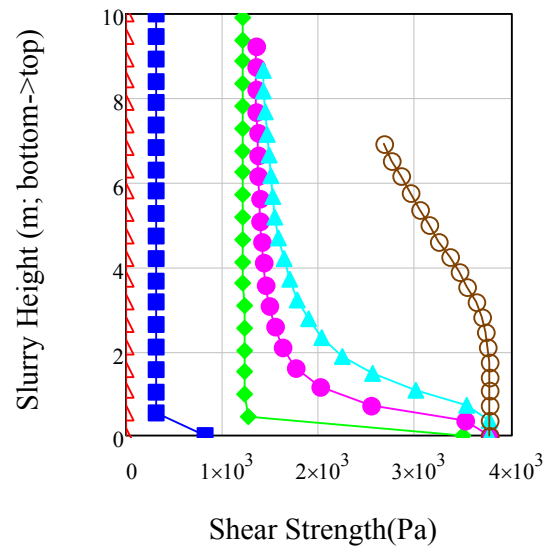
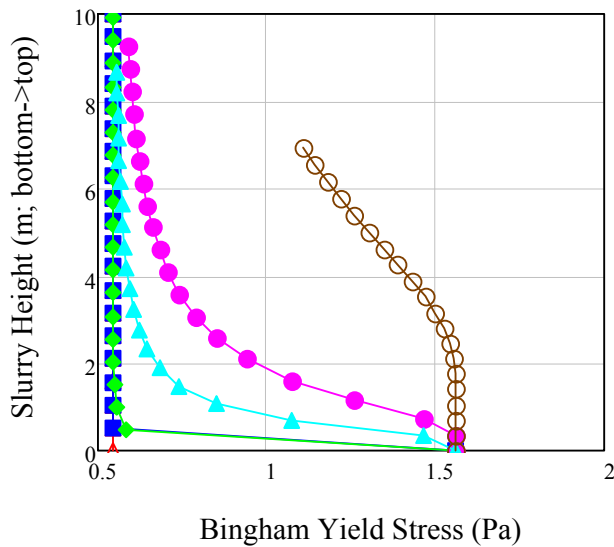
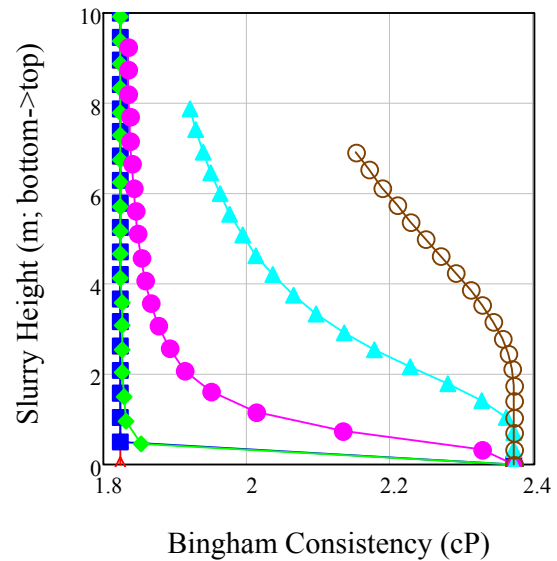
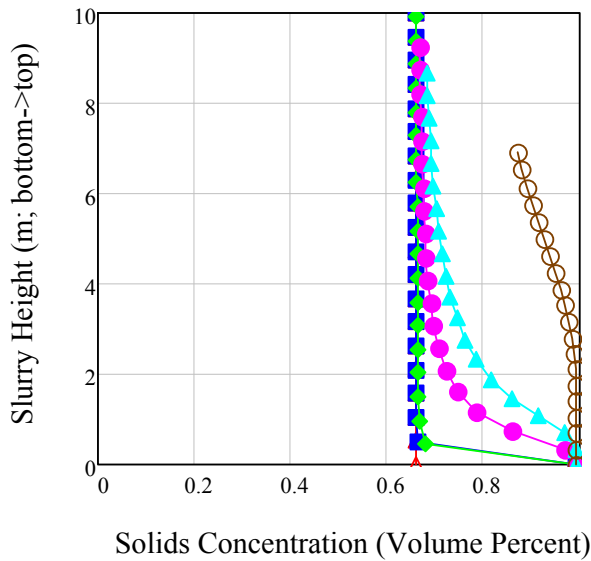


- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- ⊖⊖ 1000 hr

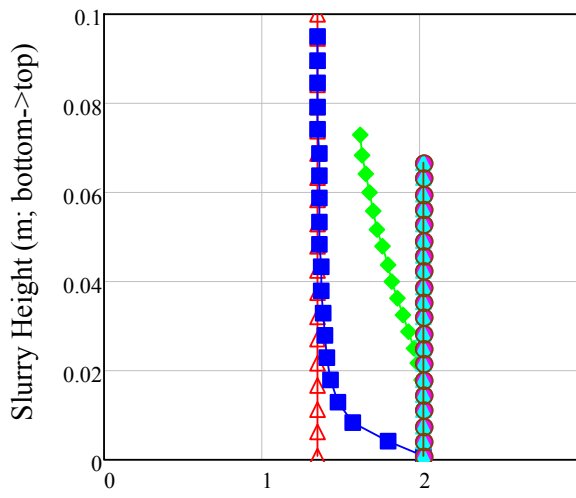


- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- ⊖⊖ 1000 hr

Predicted sludge properties from Hanford Tank T-203 with water dilution at a starting slurry height of 10 m with 33% volume excess supernatant from fully settled configuration; rheological properties taken at a temperature range of 20°–35°C.

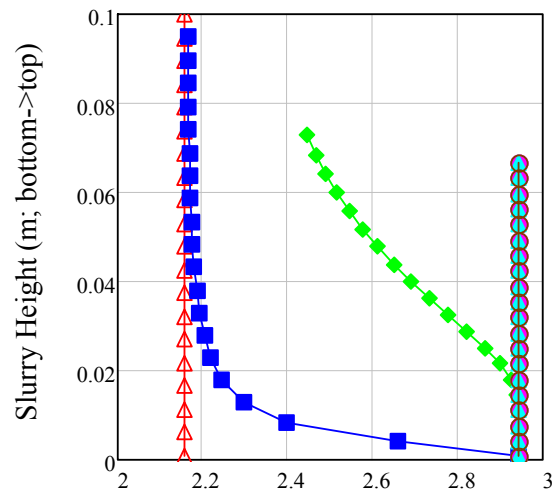


Predicted sludge properties from Hanford Tank T-110 with water dilution at a starting slurry height of 0.1 m with 33% volume excess supernatant from fully settled configuration; rheological properties taken at a temperature range of 20°–35°C.



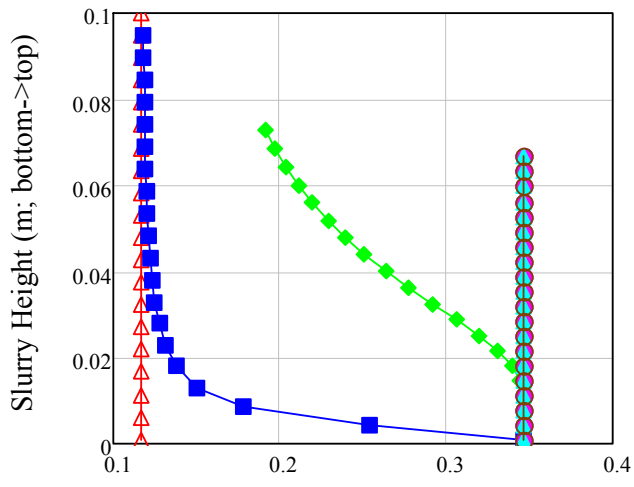
Solids Concentration (Volume Percent)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- ⊖⊖ 1000 hr



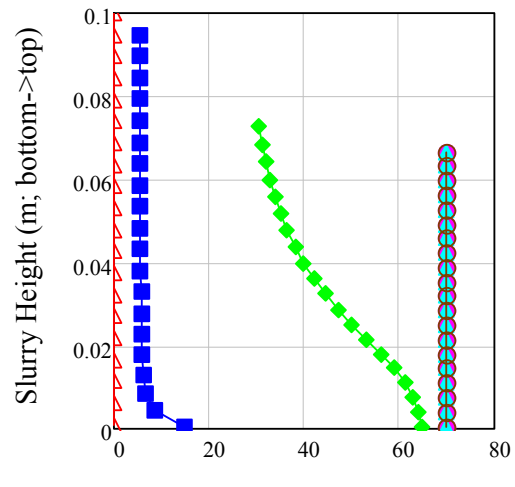
Bingham Consistency (cP)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- ⊖⊖ 1000 hr



Bingham Yield Stress (Pa)

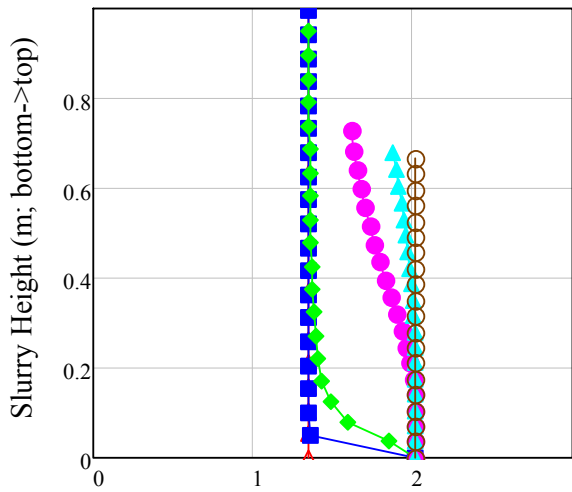
- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- ⊖⊖ 1000 hr



Shear Strength(Pa)

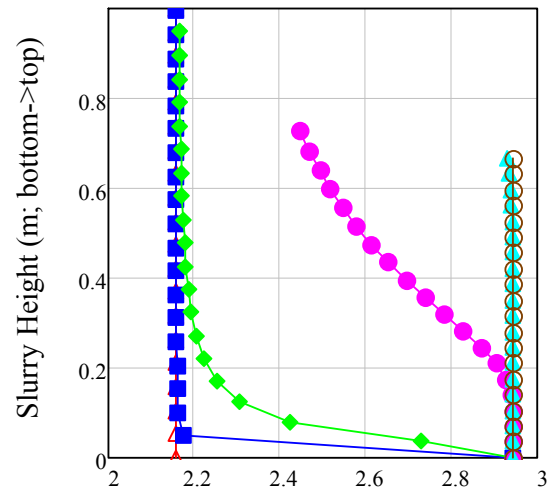
- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- ⊖⊖ 1000 hr

Predicted sludge properties from Hanford Tank T-110 with water dilution at a starting slurry height of 1 m with 33% volume excess supernatant from fully settled configuration; rheological properties taken at a temperature range of 20°–35°C.



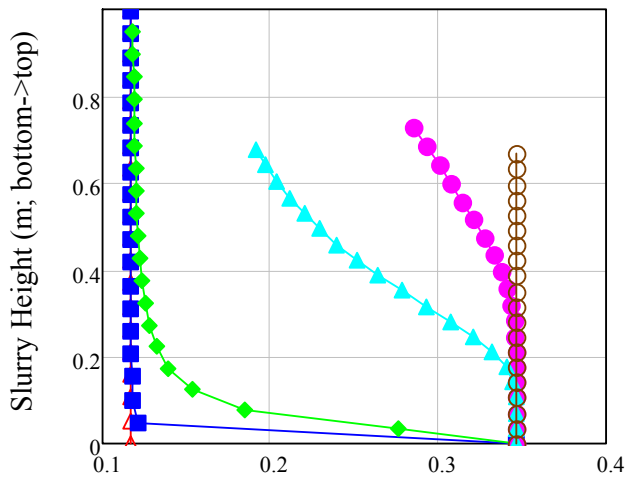
Solids Concentration (Volume Percent)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



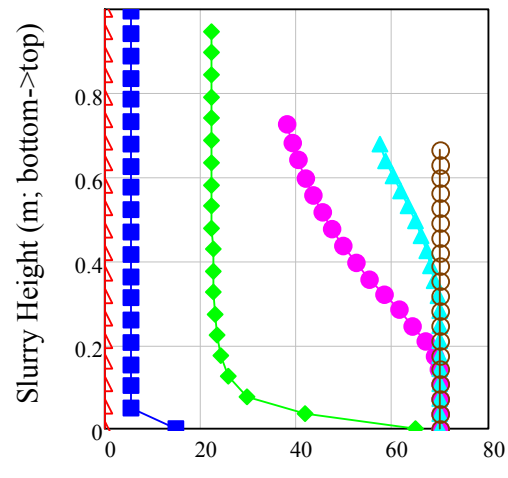
Bingham Consistency (cP)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



Bingham Yield Stress (Pa)

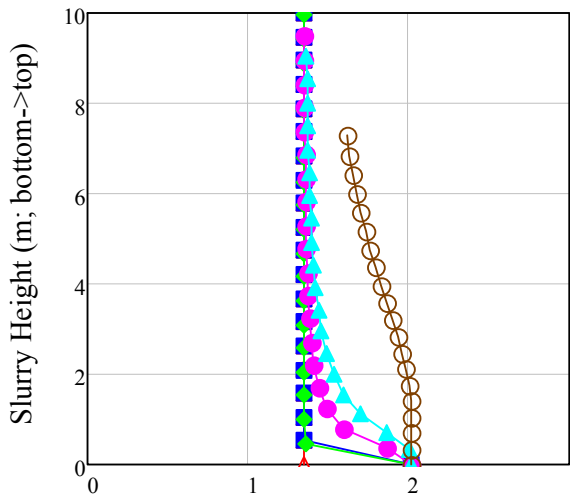
- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



Shear Strength(Pa)

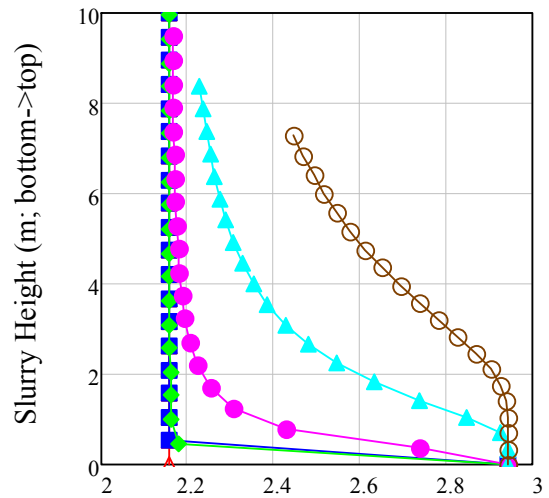
- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr

Predicted sludge properties from Hanford Tank T-110 with water dilution at a starting slurry height of 10 m with 33% volume excess supernatant from fully settled configuration; rheological properties taken at a temperature range of 20°–35°C.



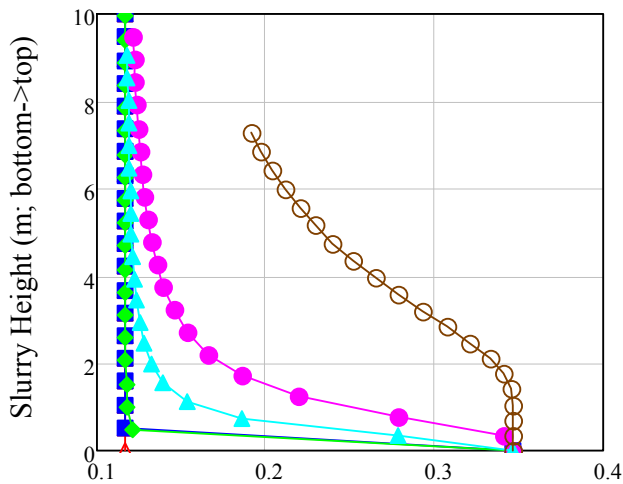
Solids Concentration (Volume Percent)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



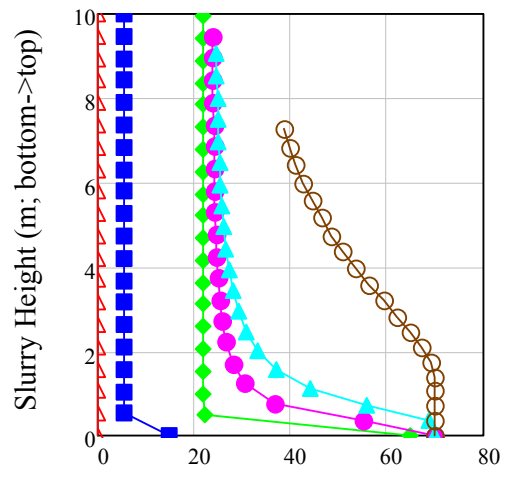
Bingham Consistency (cP)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



Bingham Yield Stress (Pa)

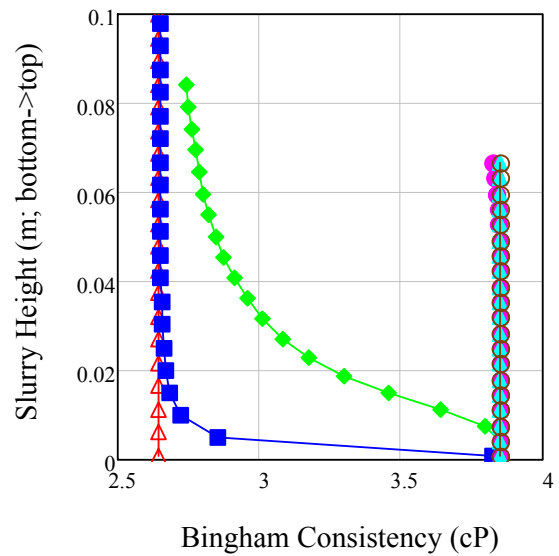
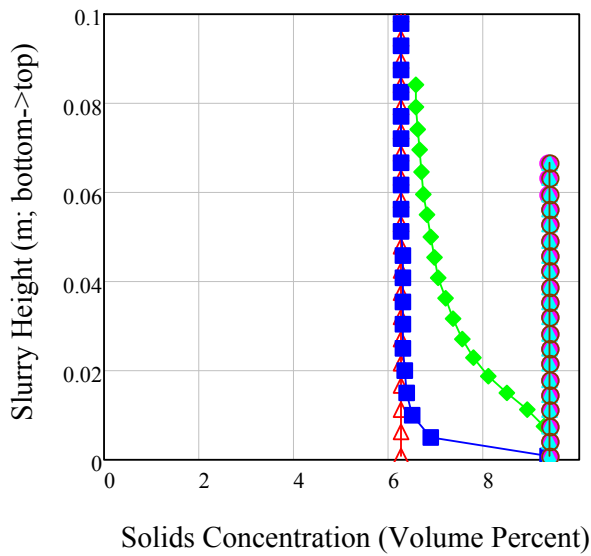
- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



Shear Strength(Pa)

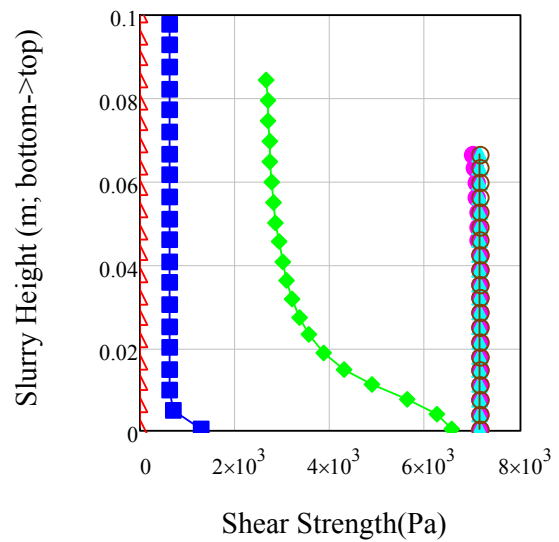
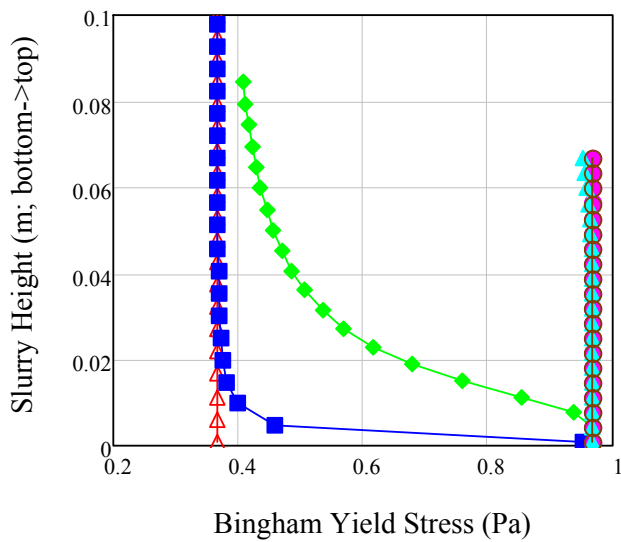
- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr

Predicted sludge properties from Hanford Tank C-104 without water dilution at a starting slurry height of 0.1 m with 33% volume excess supernatant from fully settled configuration; rheological properties taken at a temperature range of 20°–35°C.



- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- ⊖⊖ 1000 hr

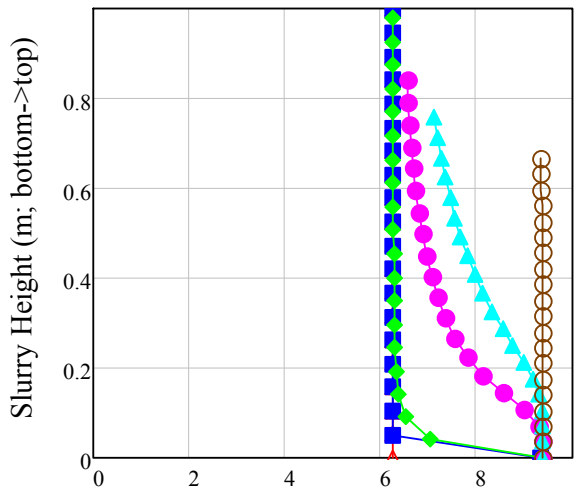
- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- ⊖⊖ 1000 hr



- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- ⊖⊖ 1000 hr

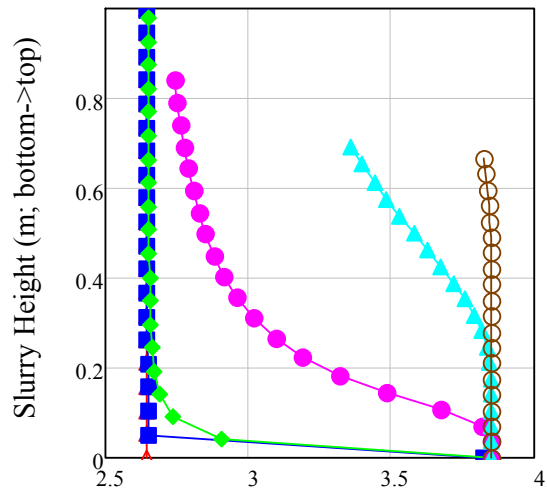
- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- ⊖⊖ 1000 hr

Predicted sludge properties from Hanford Tank C-104 without water dilution at a starting slurry height of 1 m with 33% volume excess supernatant from fully settled configuration; rheological properties taken at a temperature range of 20°–35°C.



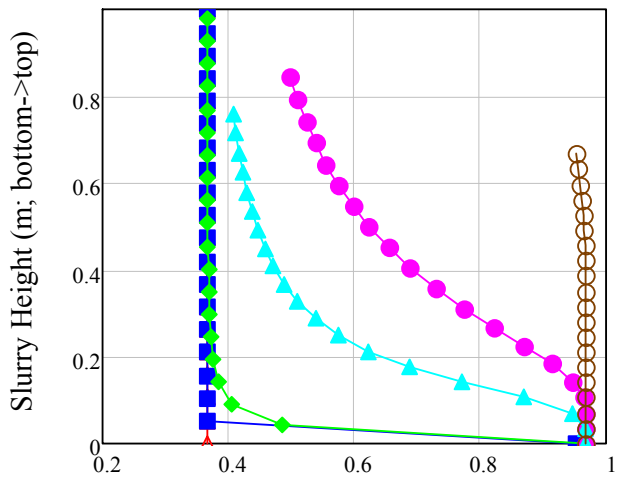
Solids Concentration (Volume Percent)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



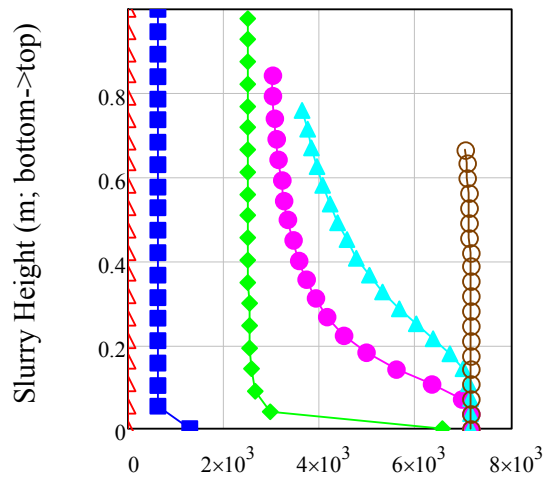
Bingham Consistency (cP)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



Bingham Yield Stress (Pa)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr

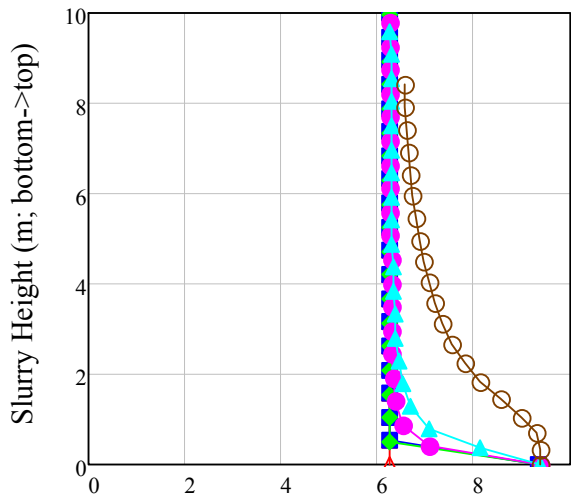


Shear Strength (Pa)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr

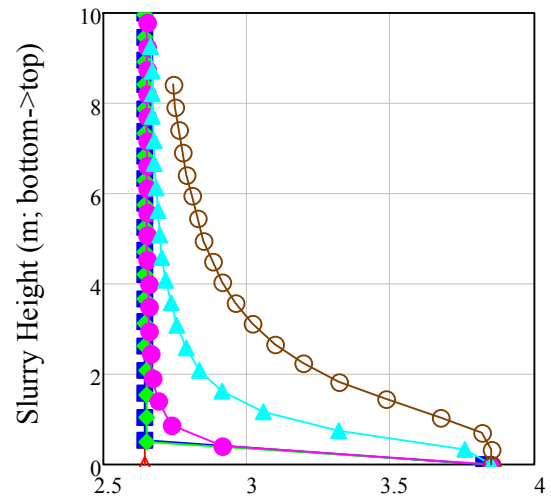


Predicted sludge properties from Hanford Tank C-104 without water dilution at a starting slurry height of 10 m with 33% volume excess supernatant from fully settled configuration; rheological properties taken at a temperature range of 20°–35°C.



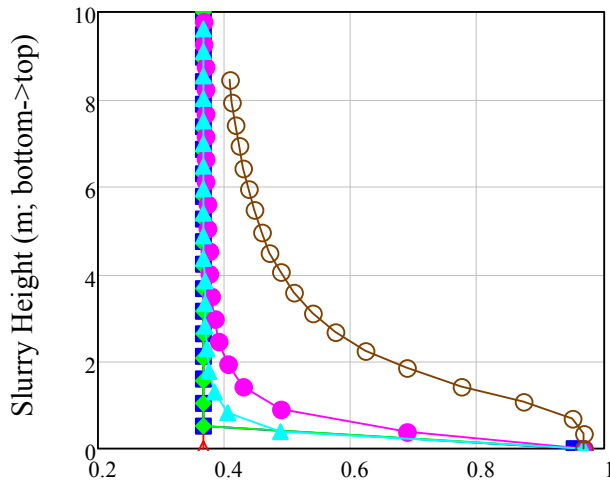
Solids Concentration (Volume Percent)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



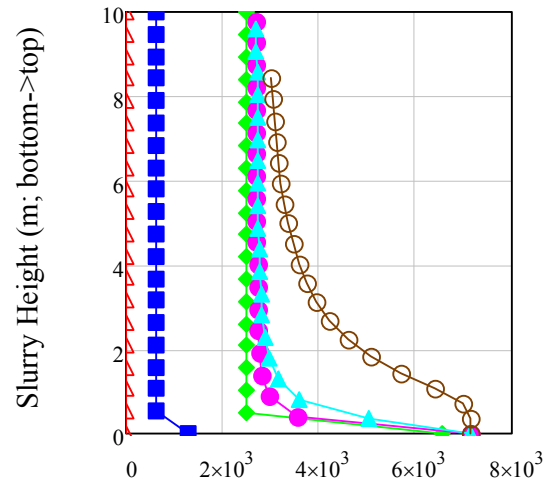
Bingham Consistency (cP)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



Bingham Yield Stress (Pa)

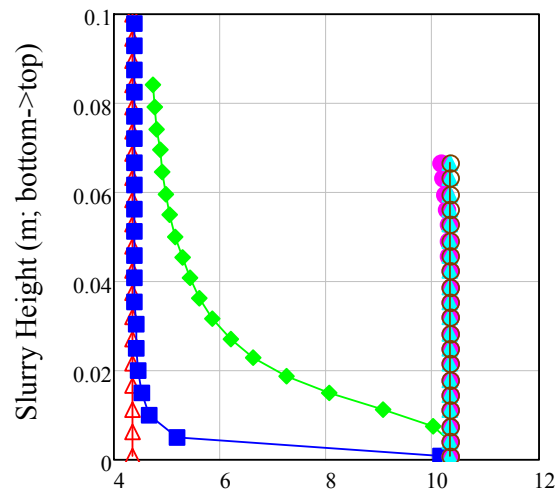
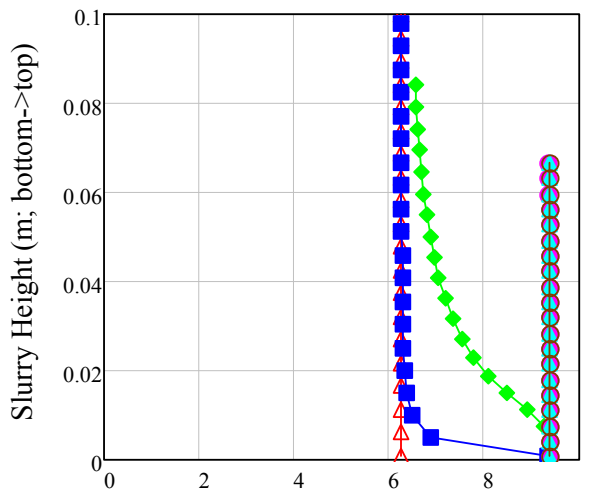
- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



Shear Strength(Pa)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr

Predicted sludge properties from Hanford Tank C-104 with water dilution at a starting slurry height of 0.1 m with 33% volume excess supernatant from fully settled configuration; rheological properties taken at a temperature range of 20°–35°C.

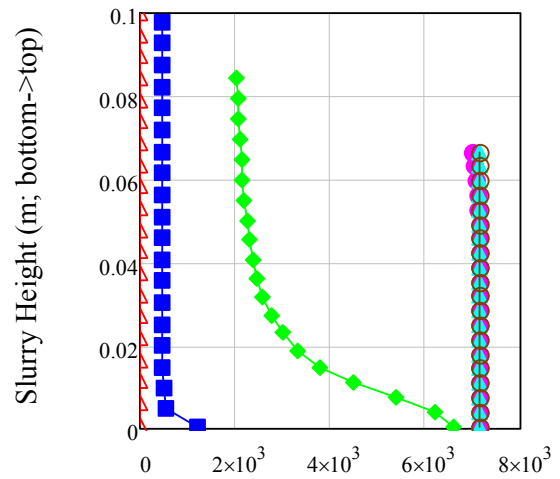
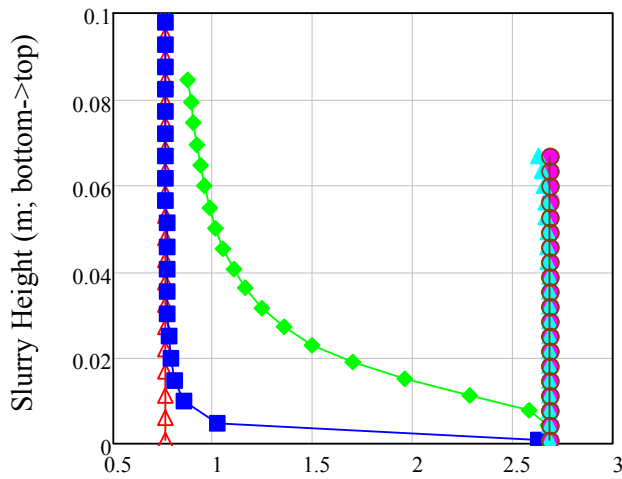


Solids Concentration (Volume Percent)

Bingham Consistency (cP)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- ⊖⊖ 1000 hr

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- ⊖⊖ 1000 hr



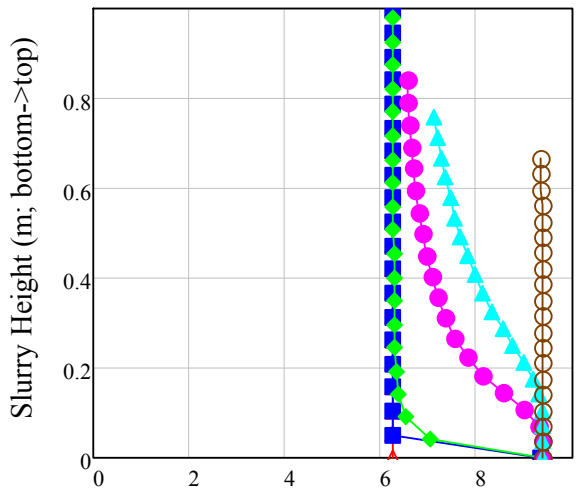
Bingham Yield Stress (Pa)

Shear Strength(Pa)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- ⊖⊖ 1000 hr

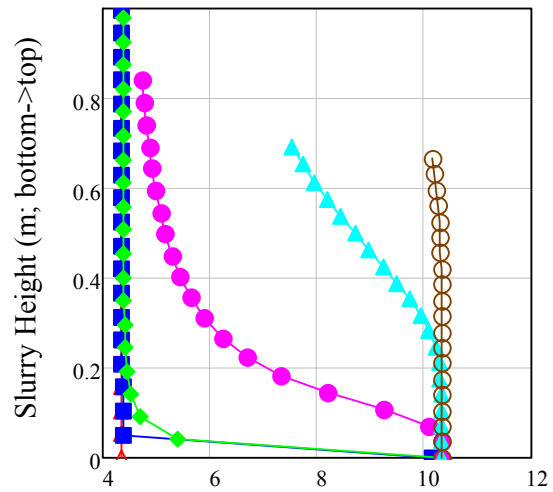
- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- ⊖⊖ 1000 hr

Predicted sludge properties from Hanford Tank C-104 with water dilution at a starting slurry height of 1 m with 33% volume excess supernatant from fully settled configuration; rheological properties taken at a temperature range of 20°–35°C.



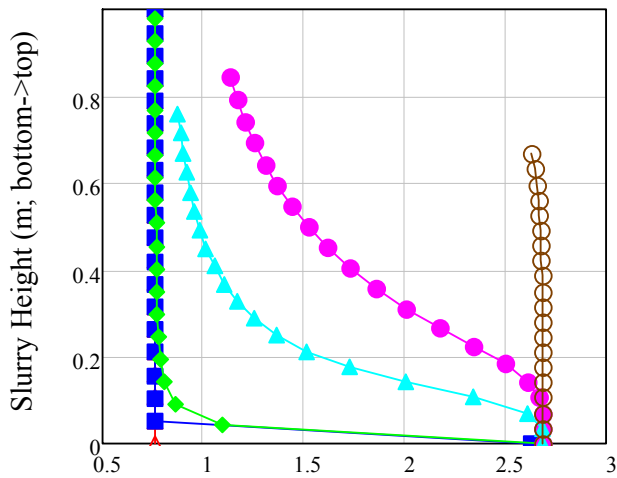
Solids Concentration (Volume Percent)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



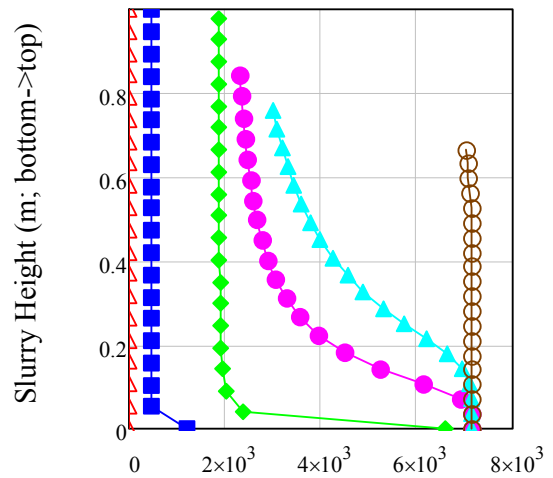
Bingham Consistency (cP)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



Bingham Yield Stress (Pa)

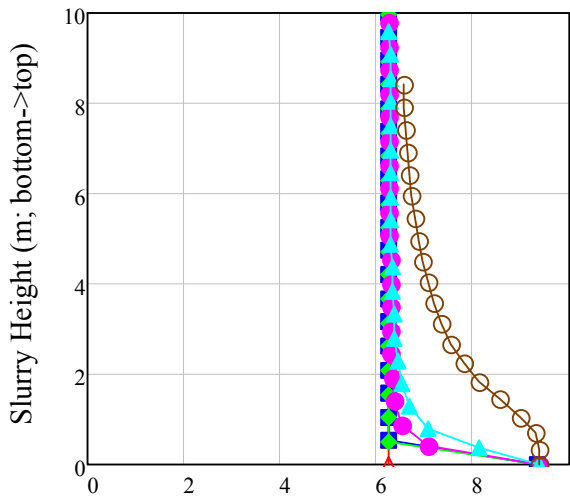
- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



Shear Strength (Pa)

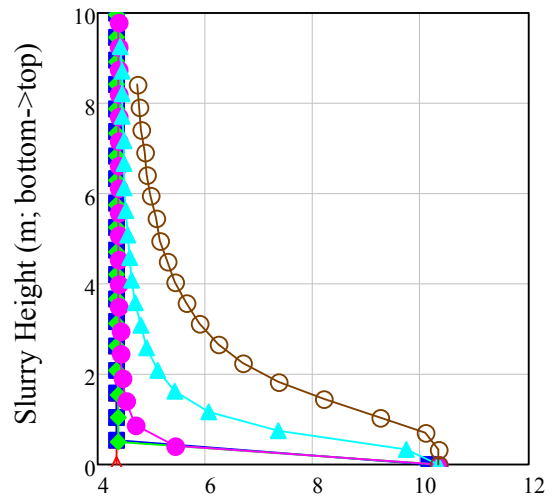
- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr

Predicted sludge properties from Hanford Tank C-104 with water dilution at a starting slurry height of 10 m with 33% volume excess supernatant from fully settled configuration; rheological properties taken at a temperature range of 20°–35°C.



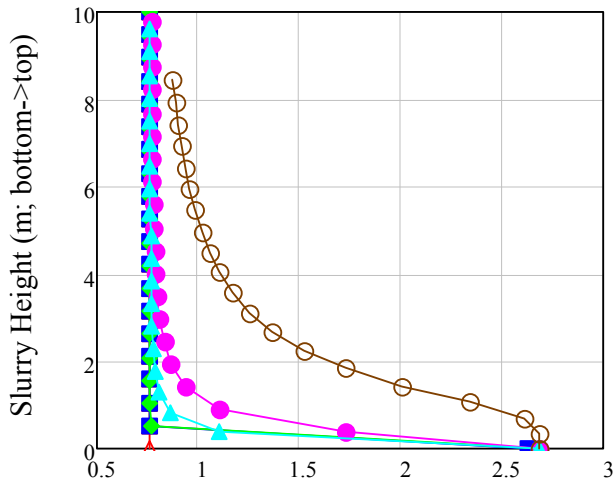
Solids Concentration (Volume Percent)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



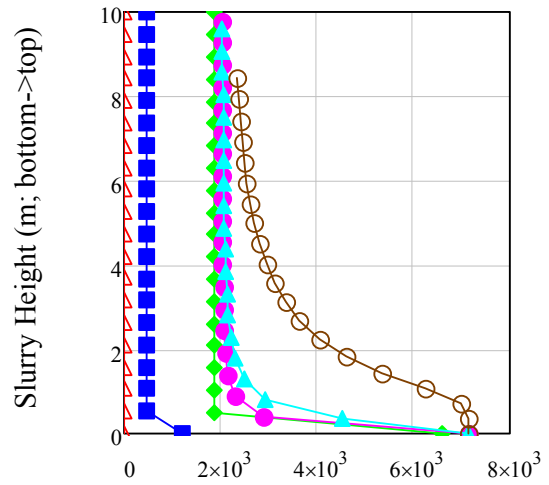
Bingham Consistency (cP)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



Bingham Yield Stress (Pa)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr



Shear Strength(Pa)

- △△ 0 hr
- 1 hr
- ◆◆ 10 hr
- 100 hr
- ▲▲ 200 hr
- 1000 hr

Model Chemical Data From ESP

Analyte/Sample	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101
Description	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ
Model Basis	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty
Source of Data	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249
Solid Phases (vol% of bulk)																	
(NaAlO <sub>2</sub> ) <sub>2</sub> ·2.5H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Bi <sub>2</sub> O <sub>3</sub>	0.00102	0.00239	0.00239	0.00239	0.00239	0.00239	0.00239	0.00239	0.00239	0.00161	0.00161	0.00239	0.00239	0.00239	0.00239	0.00239	0.00239
BiOCl	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Boehmite	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca <sub>3</sub> (OH)(PO <sub>3</sub> ) <sub>2</sub>	0.02439	0.05692	0.05692	0.05692	0.05692	0.05692	0.05692	0.05692	0.05692	0.03833	0.03833	0.05692	0.05692	0.05692	0.05692	0.05692	0.05692
Ca <sub>2</sub> C <sub>2</sub> O <sub>4</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaF <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Cr(OH) <sub>3</sub>	0.07226	0.16861	0.16861	0.16861	0.16861	0.16861	0.16861	0.16861	0.16861	0.11356	0.11356	0.16861	0.16861	0.16861	0.16861	0.16861	0.16861
Fe(OH) <sub>3</sub>	0.01650	0.03850	0.03850	0.03850	0.03850	0.03850	0.03850	0.03850	0.03850	0.02593	0.02593	0.03850	0.03850	0.03850	0.03850	0.03850	0.03850
Gibbsite	0.20629	0.48134	0.48134	0.48134	0.48134	0.48134	0.48134	0.48134	0.48134	0.32417	0.32417	0.48134	0.48134	0.48134	0.48134	0.48134	0.48134
HgO	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
KAlSiO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
La(OH) <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
LaPO <sub>4</sub> ·2H <sub>2</sub> O	0.00121	0.00283	0.00283	0.00283	0.00283	0.00283	0.00283	0.00283	0.00283	0.00191	0.00191	0.00283	0.00283	0.00283	0.00283	0.00283	0.00283
Mn(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Mn <sub>2</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
MnCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	0.01864	0.04348	0.04348	0.04348	0.04348	0.04348	0.04348	0.04348	0.04348	0.02928	0.02928	0.04348	0.04348	0.04348	0.04348	0.04348	0.04348
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaAlSiO <sub>4</sub>	0.13427	0.31329	0.31329	0.31329	0.31329	0.31329	0.31329	0.31329	0.31329	0.21099	0.21099	0.31329	0.31329	0.31329	0.31329	0.31329	0.31329
Ni(OH) <sub>2</sub>	0.00465	0.01085	0.01085	0.01085	0.01085	0.01085	0.01085	0.01085	0.01085	0.00731	0.00731	0.01085	0.01085	0.01085	0.01085	0.01085	0.01085
Ni <sub>2</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NiC <sub>2</sub> O <sub>4</sub> ·2H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pb(OH) <sub>2</sub>	0.00291	0.00680	0.00680	0.00680	0.00680	0.00680	0.00680	0.00680	0.00680	0.00458	0.00458	0.00680	0.00680	0.00680	0.00680	0.00680	0.00680
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
PbCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pu(OH) <sub>3</sub>	0.00002	0.00004	0.00004	0.00004	0.00004	0.00004	0.00004	0.00004	0.00004	0.00002	0.00002	0.00004	0.00004	0.00004	0.00004	0.00004	0.00004
SiO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
SrCO <sub>3</sub>	0.00082	0.00192	0.00192	0.00192	0.00192	0.00192	0.00192	0.00192	0.00192	0.00130	0.00130	0.00192	0.00192	0.00192	0.00192	0.00192	0.00192
TcO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
ZrO <sub>2</sub>	0.00116	0.00270	0.00270	0.00270	0.00270	0.00270	0.00270	0.00270	0.00270	0.00182	0.00182	0.00270	0.00270	0.00270	0.00270	0.00270	0.00270
KNO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	0.74255	1.73262	1.73262	1.73262	1.73262	1.73262	1.73262	1.73262	1.73262	1.16687	1.16687	1.73262	1.73262	1.73262	1.73262	1.73262	1.73262
Na <sub>2</sub> CO <sub>3</sub> ·H <sub>2</sub> O	4.54336	10.60117	10.60117	10.60117	10.60117	10.60117	10.60117	10.60117	10.60117	7.13956	7.13956	10.60117	10.60117	10.60117	10.60117	10.60117	10.60117
Na <sub>2</sub> SO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> FSO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> NO <sub>3</sub> SO <sub>4</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> ·8H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>6</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	1.10472	2.57769	2.57769	2.57769	2.57769	2.57769	2.57769	2.57769	2.57769	1.73600	1.73600	2.57769	2.57769	2.57769	2.57769	2.57769	2.57769
NaF	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF(PO <sub>3</sub> ) <sub>2</sub> ·19H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaHCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>3</sub>	5.07169	11.83394	11.83394	11.83394	11.83394	11.83394	11.83394	11.83394	11.83394	7.96980	7.96980	11.83394	11.83394	11.83394	11.83394	11.83394	11.83394
Na <sub>3</sub> PO <sub>4</sub> ·0.25NaOH·12H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Total Volume % UDS	11.95	27.88	27.88	27.88	27.88	27.88	27.88	27.88	27.88	18.77	18.77	27.88	27.88	27.88	27.88	27.88	27.88
Solids Concentration (g/L)	278.8	650.6	650.6	650.6	650.6	650.6	650.6	650.6	650.6	438.1	438.1	650.6	650.6	650.6	650.6	650.6	650.6

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Physical Property Data**

Physical Property	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101
Source of Data																
Temperature (°C)	32 - 37	32 - 37	32 - 37	32 - 37	32 - 37	32 - 37	32 - 37	32 - 37	32 - 37	32 - 37	32 - 37	32 - 37	32 - 37	32 - 37	32 - 37	32 - 37
Zeta Potential (mV)																
Bulk Density (g/mL)	1.56	1.70	1.70	1.70	1.70	1.70	1.70	1.70	1.62	1.62	1.70	1.70	1.70	1.70	1.70	1.70
vol% Settled Solids																
Density of Centrifuged Solids (g/mL)																
vol% Centrifuged Solids																
wt% Centrifuged Solids																
Supernatant Density (g/mL)	1.46	1.46	1.46	1.46	1.46	1.46	1.46	1.46	1.46	1.46	1.46	1.46	1.46	1.46	1.46	1.46
Density of Settled Solids (g/mL)																
wt% Settled Supernatant																
wt% dissolved solids in supernatant																
wt% total solids in Centrifuged Sludge																
wt% Total Solids																
wt% UDS	17.87	38.27	38.27	38.27	38.27	38.27	38.27	38.27	27.05	27.05	38.27	38.27	38.27	38.27	38.27	38.27
Density of Solids (g/cc)	2.33	2.33	2.33	2.33	2.33	2.33	2.33	2.33	2.33	2.33	2.33	2.33	2.33	2.33	2.33	2.33

Shear Strength Data

Shear Strength Schedule	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101	A-101
Source of Data	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249
Instrumentation	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer
Temperature (°C)	63	63	62	62	54	49	47	44	63	62	62	62	58	57	54	49	44
Description	Riser 15 Depth from bottom of tank is 175 inches Floating Solids	Riser 15 Depth from bottom of tank is 195 inches Floating Solids	Riser 15 Floating Solids Depth from bottom of tank is 232 inches	Riser 15 Floating Solids Depth from bottom of tank is 255 inches	Riser 15 Floating Solids Depth from bottom of tank is 295 inches	Riser 15 Floating Solids Depth from bottom of tank is 312 inches	Riser 15 Floating Solids Depth from bottom of tank is 325 inches	Riser 15 Floating Solids Depth from bottom of tank is 335 inches	Riser 24 Floating Solids Depth from bottom of tank is 180 inches	Riser 24 Floating Solids Depth from bottom of tank is 218 inches	Riser 24 Floating Solids Depth from bottom of tank is 237 inches	Riser 24 Floating Solids Depth from bottom of tank is 255 inches	Riser 24 Floating Solids Depth from bottom of tank is 270 inches	Riser 24 Floating Solids Depth from bottom of tank is 280 inches	Riser 24 Floating Solids Depth from bottom of tank is 295 inches	Riser 24 Floating Solids Depth from bottom of tank is 312 inches	Riser 24 Floating Solids Depth from bottom of tank is 345 inches
Gelation Time/Shear Strength (Pa)																	
5 minutes																	
10 minutes																	
15 minutes																	
20 minutes																	
30 minutes																	
40 minutes																	
50 minutes																	
1 hour																	
2 hours																	
3 hours																	
4 hours																	
5 hours																	
6 hours																	
24 hours																	
32 hours																	
48 hours																	
56 hours																	
72 hours																	
Infinite time (GRE)	110	700	480	220	270	440	110	400	60	360	600	700	400	400	670	630	25

## Model Chemical Data From ESP

Analyte/Sample	AN-102	AN-102	AN-102
Description	as received	as received	as received
Model Basis	Salty	Salty	Salty
Report No/Source of Data	WTP-RPT-021 Rev. 1	WTP-RPT-021 Rev. 1	WTP-RPT-021 Rev. 1
<b>Solid Phases (vol% of bulk)</b>			
(NaAlO <sub>2</sub> ) <sub>2</sub> ·2.5H <sub>2</sub> O	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	-	-	-
Bi <sub>2</sub> O <sub>3</sub>	<i>0.00010</i>	<i>0.00010</i>	<i>0.00010</i>
BiOCl	-	-	-
Boehmite	-	-	-
Ca(OH) <sub>2</sub>	-	-	-
Ca <sub>3</sub> OH(PO <sub>3</sub> ) <sub>3</sub>	<i>0.00898</i>	<i>0.00898</i>	<i>0.00898</i>
CaC <sub>2</sub> O <sub>4</sub> ·H <sub>2</sub> O	-	-	-
CaCO <sub>3</sub>	-	-	-
CaF <sub>2</sub>	-	-	-
Cr <sub>2</sub> OOH	<i>0.00116</i>	<i>0.00116</i>	<i>0.00116</i>
FeOOH	<i>0.00187</i>	<i>0.00187</i>	<i>0.00187</i>
Gibbsite	<i>0.22125</i>	<i>0.22125</i>	<i>0.22125</i>
HgO	-	-	-
KAlSiO <sub>4</sub>	-	-	-
La(OH) <sub>3</sub>	-	-	-
LaPO <sub>4</sub> ·2H <sub>2</sub> O	<i>0.00003</i>	<i>0.00003</i>	<i>0.00003</i>
Mn(OH) <sub>2</sub>	<i>0.00008</i>	<i>0.00008</i>	<i>0.00008</i>
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-
MnCO <sub>3</sub>	-	-	-
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	<i>0.00085</i>	<i>0.00085</i>	<i>0.00085</i>
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	-	-	-
NaAlSiO <sub>4</sub>	-	-	-
Ni(OH) <sub>2</sub>	<i>0.00267</i>	<i>0.00267</i>	<i>0.00267</i>
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-
NiC <sub>2</sub> O <sub>4</sub> ·2H <sub>2</sub> O	-	-	-
Pb(OH) <sub>2</sub>	<i>0.00043</i>	<i>0.00043</i>	<i>0.00043</i>
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-
PbCO <sub>3</sub>	-	-	-
Pu(OH) <sub>4</sub>	<i>0.00000</i>	<i>0.00000</i>	<i>0.00000</i>
SiO <sub>2</sub>	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-
SrCO <sub>3</sub>	<i>0.00006</i>	<i>0.00006</i>	<i>0.00006</i>
TcO <sub>2</sub>	<i>0.00000</i>	<i>0.00000</i>	<i>0.00000</i>
ZrO <sub>2</sub>	<i>0.00026</i>	<i>0.00026</i>	<i>0.00026</i>
KNO <sub>3</sub>	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	<i>0.11439</i>	<i>0.11439</i>	<i>0.11439</i>
Na <sub>2</sub> CO <sub>3</sub> ·H <sub>2</sub> O	<i>0.30599</i>	<i>0.30599</i>	<i>0.30599</i>
Na <sub>2</sub> SO <sub>4</sub>	-	-	-
Na <sub>2</sub> SO <sub>4</sub> ·10H <sub>2</sub> O	-	-	-
Na <sub>2</sub> FSO <sub>4</sub>	<i>0.08019</i>	<i>0.08019</i>	<i>0.08019</i>
Na <sub>2</sub> NO <sub>3</sub> SO <sub>3</sub> ·H <sub>2</sub> O	-	-	-
Na <sub>3</sub> PO <sub>4</sub> ·8H <sub>2</sub> O	-	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> ·10H <sub>2</sub> O	-	-	-
Na <sub>4</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	<i>0.04604</i>	<i>0.04604</i>	<i>0.04604</i>
NaF	-	-	-
NaF(PO <sub>3</sub> ) <sub>2</sub> ·19H <sub>2</sub> O	-	-	-
NaHCO <sub>3</sub>	-	-	-
NaNO <sub>2</sub>	-	-	-
NaNO <sub>3</sub>	<i>0.66221</i>	<i>0.66221</i>	<i>0.66221</i>
Na <sub>3</sub> PO <sub>4</sub> ·0.25NaOH·12H <sub>2</sub> O	-	-	-
Total Volume % UDS	<i>1.4</i>	<i>1.4</i>	<i>1.4</i>
Solids Concentration (g/L)	<b>33.9</b>	<b>33.9</b>	<b>33.9</b>



**Rheological Data**

Model/model Parameter	AN-102	AN-102	AN-102
Temperature (°C)	25	35	50
Source of Data	WTP-RPT-021 Rev. 1	WTP-RPT-021 Rev. 1	WTP-RPT-021 Rev. 1
Notes			
<b>Newtonian:</b>			
$\eta$ - Newtonian viscosity (cP)	n/m	n/m	n/m
$r$ - correlation coefficient	n/m	n/m	n/m
<b>Oswald (or Power Law):</b>			
$m$ - the consistency coefficient (Pa·s <sup><i>n</i></sup> )	0.05943	0.08108	0.05002
$n$ - the power-law exponent	0.8135	0.7081	0.7581
$r$ - correlation coefficient	1	0.97	0.98
<b>Bingham Plastic:</b>			
$\tau_B$ - the Bingham yield stress (Pa)	1.592	1.39	0.7177
$\eta_p$ - the plastic viscosity (Pa·s)	0.0147	0.0099	0.0094
$r$ - correlation coefficient	0.98	0.98	0.99
<b>Herschel-Bulkley:</b>			
$\tau_{0f}$ - the yield stress (Pa)	0.84	0.2102	0.2362
$k$ - the Herschel-Bulkely consistency coefficient (Pa·s <sup><i>n</i></sup> )	0.04164	0.03547	0.0158
$b$ - the Herschel-Bulkely power-law exponent	0.8666	0.8358	0.9362
$r$ - correlation coefficient	1	0.91	1
n/a = not applicable			

**Physical Property Data**

Physical Property	AN-102	AN-102	AN-102
Notes	WTP-RPT-021 Table 4.4	WTP-RPT-021 Table 4.4	WTP-RPT-021 Table 4.4
Temperature (°C)			
Zeta Potential (mV)			
Bulk Density (g/mL)	1.411	1.411	1.411
vol% Settled Solids	22	22	22
Density of Centrifuged Solids (g/mL)	1.49	1.49	1.49
vol% Centrifuged Solids	13.4	13.4	13.4
wt% Centrifuged Solids	14.1	14.1	14.1
Supernatant Density (g/mL)	<b>1.40</b>	<b>1.40</b>	<b>1.40</b>
Density of Settled Solids (g/mL)	n/m	n/m	n/m
wt% Settled Supernatant	n/m	n/m	n/m
wt% dissolved solids in supernatant	51.5	51.5	51.5
wt% total solids in Centrifuged Sludge	52.9	52.9	52.9
wt% Total Solids			
wt% UDS	2.4	2.4	2.4
Density of Solids (g/cc)	<b>2.34</b>	<b>2.34</b>	<b>2.34</b>







Model Chemical Data From ESP

Analyte/Sample	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104
Description	permeate	concentrated slurry	water washed slurry	Undiluted WTC	Undiluted WTC	Undiluted WTC	WTC 50% dilution	WTC 50% dilution	WTC 50% dilution	Settled Solids 80% Dilution	Settled Solids 80% Dilution	Settled Solids 80% Dilution	Undiluted Settled Solids	Undiluted Settled Solids	Undiluted Settled Solids	Undiluted Supernate Liquid	Undiluted Supernate Liquid
Model Basis	Salty	Salty	Salt Free	Salty	Salty	Salty	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free	Salty	Salty
Report No./Source of Data	WSRC-TR-2003-00295, REV. 0	WSRC-TR-2003-00295, REV. 0	WSRC-TR-2003-00295, REV. 0	HNF-3352	HNF-3352	HNF-3352	HNF-3352	HNF-3352	HNF-3352	HNF-3352	HNF-3352	HNF-3352	HNF-3352	HNF-3352	HNF-3352	HNF-3352	HNF-3352
Solid Phases (wt% of bulk)																	
(NaAlO <sub>2</sub> ) <sub>2</sub> ·2.5H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Bi <sub>2</sub> O <sub>3</sub>	-	0.0001	0.00159	0.00009	0.00009	0.00009	0.00207	0.00207	0.00207	0.00086	0.00086	0.00086	0.01059	0.01059	0.01059	-	-
BiOCl	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Boehmite	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca <sub>2</sub> OH(PO <sub>3</sub> ) <sub>3</sub>	-	0.00068	0.07822	0.00435	0.00435	0.00435	0.10136	0.10136	0.10136	0.04239	0.04239	0.04239	0.51972	0.51972	0.51972	-	-
Ca <sub>2</sub> C <sub>2</sub> O <sub>4</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaF <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CrOOH	-	0.00168	0.19226	0.01068	0.01068	0.01068	0.24914	0.24914	0.24914	0.10421	0.10421	0.10421	1.27751	1.27751	1.27751	-	-
FeOOH	-	0.00017	0.01942	0.00108	0.00108	0.00108	0.02516	0.02516	0.02516	0.01053	0.01053	0.01053	0.12904	0.12904	0.12904	-	-
Gibbsite	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
HgO	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
KAlSiO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
La(OH) <sub>3</sub>	-	0.00008	0.00959	0.00053	0.00053	0.00053	0.01243	0.01243	0.01243	0.00520	0.00520	0.00520	0.06372	0.06372	0.06372	-	-
LaPO <sub>4</sub> ·2H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Mn(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Mn <sub>2</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
MnCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	-	0.00014	0.01624	0.00090	0.00090	0.00090	0.02104	0.02104	0.02104	0.00880	0.00880	0.00880	0.10790	0.10790	0.10790	-	-
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaAlSiO <sub>4</sub>	-	0.00303	0.34688	0.01927	0.01927	0.01927	0.44950	0.44950	0.44950	0.18801	0.18801	0.18801	2.30487	2.30487	2.30487	-	-
Ni(OH) <sub>2</sub>	-	0.00007	0.00047	0.00047	0.00047	0.00047	0.01091	0.01091	0.01091	0.00456	0.00456	0.00456	0.05594	0.05594	0.05594	-	-
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NiC <sub>2</sub> O <sub>4</sub> ·2H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pb(OH) <sub>2</sub>	-	0.00004	0.00448	0.00025	0.00025	0.00025	0.00580	0.00580	0.00580	0.00243	0.00243	0.00243	0.02974	0.02974	0.02974	-	-
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
PbCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pu(OH) <sub>4</sub>	-	0.00000	0.00000	0.00000	0.00000	0.00000	0.00001	0.00001	0.00001	0.00000	0.00000	0.00000	0.00003	0.00003	0.00003	-	-
SiO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
SrCO <sub>3</sub>	-	0.00001	0.00132	0.00007	0.00007	0.00007	0.00171	0.00171	0.00171	0.00072	0.00072	0.00072	0.00877	0.00877	0.00877	-	-
TcO <sub>2</sub>	-	0.00000	0.00005	0.00000	0.00000	0.00000	0.00007	0.00007	0.00007	0.00003	0.00003	0.00003	0.00034	0.00034	0.00034	-	-
ZrO <sub>2</sub>	-	0.00000	0.00015	0.00001	0.00001	0.00001	0.00020	0.00020	0.00020	0.00008	0.00008	0.00008	0.00102	0.00102	0.00102	-	-
KNO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	-	0.01929	-	0.12258	0.12258	0.12258	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> CO <sub>3</sub> ·H <sub>2</sub> O	-	0.14796	-	0.94043	0.94043	0.94043	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> FSO <sub>4</sub>	-	0.00168	-	0.01068	0.01068	0.01068	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> NO <sub>3</sub> ·SO <sub>2</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> PO <sub>3</sub> ·8H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> P <sub>2</sub> O <sub>7</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> (SO <sub>4</sub> ) <sub>2</sub> ·CO <sub>3</sub>	-	0.02940	-	0.18686	0.18686	0.18686	-	-	-	-	-	-	-	-	-	-	-
NaF	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF(PO <sub>3</sub> ) <sub>2</sub> ·19H <sub>2</sub> O	-	0.01973	-	0.12543	0.12543	0.12543	-	-	-	-	-	-	-	-	-	-	-
NaHCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>2</sub>	-	0.00409	-	0.02597	0.02597	0.02597	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>3</sub>	-	0.27157	-	1.72611	1.72611	1.72611	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> ·0.25NaOH·12H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Total Volume % UDS	-	0.50	0.68	3.18	3.18	3.18	0.88	0.88	0.88	0.37	0.37	0.37	4.51	4.51	4.51	-	-
Solids Concentration (g/L)	-	11.4	24.3	72.4	72.4	72.4	31.5	31.5	31.5	13.2	13.2	13.2	161.6	161.6	161.6	-	-

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

Rheological Data

Model/parameter	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104
Temperature (°C)	25	25	25	25	45	65	25	45	65	25	45	65	25	45	65	25	45	65
Source of Data	WSRC-TR-2003-00295, REV. 0	WSRC-TR-2003-00295, REV. 0	WSRC-TR-2003-00295, REV. 0	HNF-3352	HNF-3352	HNF-3352	HNF-3352	HNF-3352	HNF-3352	HNF-3352	HNF-3352	HNF-3352	HNF-3352	HNF-3352	HNF-3352	HNF-3352	HNF-3352	HNF-3352
Notes				Page B7	Page B14	Page B21	Page B28	Page B35	Page B42	Page B49	Page B56	Page B63	Page B70	Page B78	Page B85	Page B92	Page B99	Page B106
<b>Newtonian:</b>																		
$\eta$ - Newtonian viscosity (cP)	3.5	3.85	n/m	2.879	14.000	7.591	8.786	5.428	4.650	27.426	12.890	7.684	56.435	25.350	15.860	16.929	8.071	4.571
$r$ - correlation coefficient	n/m	n/m	n/m	1.000	0.999	0.997	0.999	0.997	0.999	0.999	0.999	0.992	0.999	0.996	0.997	1.000	0.995	0.997
<b>Ostwald (or Power Law):</b>																		
$n$ - the consistency coefficient (Pas <sup>-n</sup> )	n/m	n/m	n/m	0.003	0.024	0.023	0.012	0.010	0.020	0.040	0.039	0.020	0.064	0.062	0.088	0.017	0.008	0.005
$n$ - the power-law exponent	n/m	n/m	n/m	0.990	0.905	0.800	0.943	0.897	0.738	0.929	0.798	0.823	0.978	0.836	0.685	1.000	1.000	1.000
$r$ - correlation coefficient	n/m	n/m	n/m	1.000	0.998	0.985	1.000	0.990	0.976	1.000	0.986	1.000	0.999	0.998	0.998	1.000	0.995	0.997
<b>Bingham Plastic:</b>																		
$\tau_B$ - the Bingham yield stress (Pa)	0	0	1.47	0.002	0.211	0.202	0.021	0.170	0.289	0.099	0.098	0.098	0.136	0.135	0.376	0.000	0.000	0.000
$\eta_p$ - the plastic viscosity (Pas)	0.0035	0.00385	0.0019	0.003	0.013	0.007	0.009	0.005	0.003	0.027	0.013	0.007	0.056	0.025	0.014	0.017	0.008	0.005
$r$ - correlation coefficient	n/m	n/m	n/m	1.000	0.999	0.997	0.999	0.997	0.997	0.999	0.999	0.992	0.999	0.996	0.979	1.000	0.995	0.997
<b>Herschel-Bulkley:</b>																		
$\tau_0$ - the yield stress (Pa)	n/m	n/m	n/m	0.000	0.198	0.194	0.010	0.169	0.291	0.000	0.000	0.003	0.001	0.001	0.001	0.001	0.000	0.000
$k$ - the Herschel-Bulkley consistency coefficient (Pas <sup>n</sup> )	n/m	n/m	n/m	0.003	0.015	0.014	0.011	0.005	0.004	0.040	0.039	0.020	0.064	0.062	0.088	0.017	0.008	0.005
$b$ - the Herschel-Bulkley power-law exponent	n/m	n/m	n/m	0.980	0.980	0.867	0.966	1.000	0.986	0.930	0.799	0.822	0.978	0.836	0.685	1.000	1.000	1.000
$r$ - correlation coefficient	n/m	n/m	n/m	1.000	0.999	0.991	1.000	0.997	0.996	1.000	0.986	1.000	0.999	0.998	0.997	1.000	0.995	0.997
n/a = not applicable																		

Physical Property Data

Physical Property	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104
Notes																		
Temperature (°C)	25	25	25	25	45	65	25	45	65	25	45	65	25	45	65	25	45	65
Zeta Potential (mV)																		
Bulk Density (g/mL)	1.26	1.27	1.11	1.45	1.45	1.45	1.33	1.33	1.33	1.32	1.32	1.32	1.52	1.52	1.52	1.42	1.42	1.42
vol% Settled Solids	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
Density of Centrifuged Solids (g/mL)	0	0	0	1.52	1.52	1.52	1.98	1.98	1.98	1.45	1.45	1.45	1.62	1.62	1.62	0	0	0
vol% Centrifuged Solids	n/m	n/m	n/m	27	27	27	3	3	3	6	6	6	50	50	50	0	0	0
wt% Centrifuged Solids	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
Supernatant Density (g/mL)	1.26	1.26	1.09	1.42	1.42	1.42	1.31	1.31	1.31	1.31	1.31	1.31	1.42	1.42	1.42	1.42	1.42	1.42
Density of Settled Solids (g/mL)	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% Settled Supernatant	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% dissolved solids in supernatant	29.3	29.1	11.6	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% total solids in Centrifuged Sludge	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% Total Solids	29.3	30	11.6	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% UDS	0	0.9	2.2	5	5	5	2.37	2.37	2.37	1	1	1	10.65	10.65	10.65	0	0	0
Density of Solids (g/cc)	2.28	2.28	3.58	2.28	2.28	2.28	3.58	3.58	3.58	3.58	3.58	3.58	3.58	3.58	3.58	2.28	2.28	2.28

**Settling Data**

Settling Schedule					<i>AN-104</i>					<i>AN-104</i>					<i>AN-104</i>					
Notes:																				
Temperature (°C)					45					45					45					
Total initial volume					30					46.5					31.2					20
5 minutes																				
10 minutes																				
15 minutes																				
20 minutes																				
30 minutes																				
40 minutes																				
50 minutes																				
1 hour															21					18.5
2 hours					25					12.5					14.5					18.5
3 hours															13.2					18.5
4 hours					18					8.2					12.5					18.5
5 hours															12					18.5
6 hours																				
24 hours					17					4.5					4.5					17
32 hours					17															
48 hours					17					4										17
56 hours					17					4										
72 hours final settled					17					4					3.5					17

**Shear Strength Data**

Shear Strength Schedule																					
Source of Data																					
Notes:																					
Temperature (°C)																					
Description																					
Gelation Time/Shear Strength (Pa)																					
5 minutes																					
10 minutes																					
15 minutes																					
20 minutes																					
30 minutes																					
40 minutes																					
50 minutes																					
1 hour																					
2 hours																					
3 hours																					
4 hours																					
5 hours																					
6 hours																					
24 hours																					
32 hours																					
48 hours																					
56 hours																					
72 hours																					
Infinite time (GRE)																					

Model Chemical Data Fr

Analyte/Sample	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	
Description	Settled Solids 80% Dilution Supernate	Settled Solids 80% Dilution Supernate	Settled Solids 80% Dilution Supernate	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	
Model Basis	Salt Free	Salt Free	Salt Free	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	
Report No./Source of Data	HNF-3352	HNF-3352	HNF-3352	RPP-6655	RPP-6655	RPP-6655	RPP-6655	RPP-6655	RPP-6655	RPP-6655	RPP-6655	RPP-6655	RPP-6655	RPP-6655	RPP-6655	
Solid Phases (vol% of bulk)	PNNL-11296	PNNL-11296	PNNL-11296	PNNL-11296	PNNL-11296	PNNL-11296	PNNL-11296	PNNL-11296	PNNL-11296	PNNL-11296	PNNL-11296	PNNL-11296	PNNL-11296	PNNL-11296	PNNL-11296	
(NaAlO <sub>2</sub> ) <sub>2</sub> ·2.5H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Bi <sub>2</sub> O <sub>3</sub>	-	-	-	0.00055	0.00055	0.00055	0.00055	0.00055	0.00055	0.00055	0.00055	0.00055	0.00055	0.00055	0.00055	0.00055
BiOCl	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Boehmite	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca <sub>2</sub> OH(PO <sub>3</sub> ) <sub>3</sub>	-	-	-	0.02709	0.02709	0.02709	0.02709	0.02709	0.02709	0.02709	0.02709	0.02709	0.02709	0.02709	0.02709	0.02709
Ca <sub>2</sub> C <sub>2</sub> O <sub>4</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaF <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CrOOH	-	-	-	0.06660	0.06660	0.06660	0.06660	0.06660	0.06660	0.06660	0.06660	0.06660	0.06660	0.06660	0.06660	0.06660
FeOOH	-	-	-	0.00673	0.00673	0.00673	0.00673	0.00673	0.00673	0.00673	0.00673	0.00673	0.00673	0.00673	0.00673	0.00673
Gibbsite	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
HgO	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
KAlSiO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
La(OH) <sub>3</sub>	-	-	-	0.00332	0.00332	0.00332	0.00332	0.00332	0.00332	0.00332	0.00332	0.00332	0.00332	0.00332	0.00332	0.00332
LaPO <sub>4</sub> ·2H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Mn(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
MnCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	-	-	-	0.00562	0.00562	0.00562	0.00562	0.00562	0.00562	0.00562	0.00562	0.00562	0.00562	0.00562	0.00562	0.00562
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaAlSiO <sub>4</sub>	-	-	-	0.12015	0.12015	0.12015	0.12015	0.12015	0.12015	0.12015	0.12015	0.12015	0.12015	0.12015	0.12015	0.12015
Ni(OH) <sub>2</sub>	-	-	-	0.00292	0.00292	0.00292	0.00292	0.00292	0.00292	0.00292	0.00292	0.00292	0.00292	0.00292	0.00292	0.00292
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NiC <sub>2</sub> O <sub>4</sub> ·2H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pb(OH) <sub>2</sub>	-	-	-	0.00155	0.00155	0.00155	0.00155	0.00155	0.00155	0.00155	0.00155	0.00155	0.00155	0.00155	0.00155	0.00155
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
PbCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pu(OH) <sub>3</sub>	-	-	-	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
SiO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
SrCO <sub>3</sub>	-	-	-	0.00046	0.00046	0.00046	0.00046	0.00046	0.00046	0.00046	0.00046	0.00046	0.00046	0.00046	0.00046	0.00046
TeO <sub>2</sub>	-	-	-	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002
ZrO <sub>2</sub>	-	-	-	0.00005	0.00005	0.00005	0.00005	0.00005	0.00005	0.00005	0.00005	0.00005	0.00005	0.00005	0.00005	0.00005
KNO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	-	-	-	0.76421	0.76421	0.76421	0.76421	0.76421	0.76421	0.76421	0.76421	0.76421	0.76421	0.76421	0.76421	0.76421
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub> ·H <sub>2</sub> O	-	-	-	5.86308	5.86308	5.86308	5.86308	5.86308	5.86308	5.86308	5.86308	5.86308	5.86308	5.86308	5.86308	5.86308
Na <sub>2</sub> SO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> FSO <sub>4</sub>	-	-	-	0.06657	0.06657	0.06657	0.06657	0.06657	0.06657	0.06657	0.06657	0.06657	0.06657	0.06657	0.06657	0.06657
Na <sub>2</sub> NO <sub>2</sub> ·SO <sub>2</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> PO <sub>3</sub> ·8H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> P <sub>2</sub> O <sub>7</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-	-	1.16495	1.16495	1.16495	1.16495	1.16495	1.16495	1.16495	1.16495	1.16495	1.16495	1.16495	1.16495	1.16495
NaF	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF(PO <sub>3</sub> ) <sub>2</sub> ·19H <sub>2</sub> O	-	-	-	0.78197	0.78197	0.78197	0.78197	0.78197	0.78197	0.78197	0.78197	0.78197	0.78197	0.78197	0.78197	0.78197
NaHCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>2</sub>	-	-	-	0.16189	0.16189	0.16189	0.16189	0.16189	0.16189	0.16189	0.16189	0.16189	0.16189	0.16189	0.16189	0.16189
NaNO <sub>3</sub>	-	-	-	10.76138	10.76138	10.76138	10.76138	10.76138	10.76138	10.76138	10.76138	10.76138	10.76138	10.76138	10.76138	10.76138
Na <sub>2</sub> PO <sub>3</sub> ·0.25NaOH·12H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Total Volume % UDS	-	-	-	19.80	19.80	19.80	19.80	19.80	19.80	19.80	19.80	19.80	19.80	19.80	19.80	19.80
Solids Concentration (g/L)	-	-	-	451.1	451.1	451.1	451.1	451.1	451.1	451.1	451.1	451.1	451.1	451.1	451.1	451.1



**Rheological Data**

Model/model Parameter	AN-104	AN-104	AN-104												
Temperature (°C)	25	45	65												
Source of Data	HNF-3352	HNF-3352	HNF-3352												
Notes	Page B113	Page B119	Page B127												
<b>Newtonian:</b>															
$\eta$ - Newtonian viscosity (cP)	17.500	8.143	5.357												
$r$ - correlation coefficient	0.999	0.998	0.999												
<b>Ostwald (or Power Law):</b>															
$m$ - the consistency coefficient (Pas <sup>-n</sup> )	0.019	0.010	0.005												
$n$ - the power-law exponent	0.989	0.963	1.000												
$r$ - correlation coefficient	0.999	0.998	0.999												
<b>Bingham Plastic:</b>															
$\tau_0$ - the Bingham yield stress (Pa)	0.000	0.010	0.000												
$\eta_p$ - the plastic viscosity (Pas)	0.017	0.008	0.005												
$r$ - correlation coefficient	0.999	0.998	0.999												
<b>Herschel-Bulkley:</b>															
$\tau_0$ - the yield stress (Pa)	0.000	0.000	0.000												
$k$ - the Herschel-Bulkely consistency coefficient (Pas <sup>n</sup> )	0.019	0.010	0.005												
$n$ - the Herschel-Bulkely power-law exponent	0.989	0.963	1.000												
$r$ - correlation coefficient	0.999	0.998	0.999												
n/a = not applicable															

**Physical Property Data**

Physical Property	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104	AN-104
Notes															
Temperature (°C)	25	45	65												
Zeta Potential (mV)															
Bulk Density (g/mL)	<i>1.31</i>	<i>1.31</i>	<i>1.31</i>	1.59	1.59	1.59	1.59	1.59	1.59	1.59	1.59	1.59	1.59	1.59	1.59
vol% Settled Solids	n/m	n/m	n/m												
Density of Centrifuged Solids (g/mL)	<i>0</i>	<i>0</i>	<i>0</i>	0	0	0	0	0	0	0	0	0	0	0	0
vol% Centrifuged Solids	n/m	n/m	n/m												
wt% Centrifuged Solids	n/m	n/m	n/m												
Supernatant Density (g/mL)	1.31	1.31	1.31	1.42	1.42	1.42	1.42	1.42	1.42	1.42	1.42	1.42	1.42	1.42	1.42
Density of Settled Solids (g/mL)	n/m	n/m	n/m												
wt% Settled Supernatant	n/m	n/m	n/m												
wt% dissolved solids in supernatant	n/m	n/m	n/m	50	50	50	50	50	50	50	50	50	50	50	50
wt% total solids in Centrifuged Sludge	n/m	n/m	n/m												
wt% Total Solids	n/m	n/m	n/m	55	55	55	55	55	55	55	55	55	55	55	55
wt% UDS	0	0	0	<i>28.37405002</i>	<i>28.37405002</i>	<i>28.37405002</i>	<i>28.37405002</i>	<i>28.37405002</i>	<i>28.37405002</i>	<i>28.37405002</i>	<i>28.37405002</i>	<i>28.37405002</i>	<i>28.37405002</i>	<i>28.37405002</i>	<i>28.37405002</i>
Density of Solids (g/cc)	3.58	3.58	3.58	2.28	2.28	2.28	2.28	2.28	2.28	2.28	2.28	2.28	2.28	2.28	2.28



Model Chemical Data From ESP

Analyte/Sample	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	
Description	Undiluted WTC	Undiluted WTC	Undiluted WTC	WTC 50% dilution	WTC 50% dilution	WTC 50% dilution	Dilution	Dilution	Dilution	Undiluted Settled Solids	Undiluted Settled Solids	Undiluted Settled Solids	Liquid	Liquid	Liquid	
Model Basis	Salty	Salty	Salty	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free	Salty	Salty	Salty	Salty	Salty	Salty	
Report No./Source of Data	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	
Solid Phases (vol% of bulk)																
(NaAlO <sub>2</sub> ) <sub>2</sub> ·2.5H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Bi <sub>2</sub> O <sub>3</sub>	0.00032	0.00032	0.00032	0.00035	0.00035	0.00035	0.00202	0.00202	0.00202	0.00041	0.00041	0.00041	-	-	-	-
BiOCl	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Boehmite	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca <sub>3</sub> (OH)(PO <sub>3</sub> ) <sub>3</sub>	0.03600	0.03600	0.03600	0.03950	0.03950	0.03950	0.23032	0.23032	0.23032	0.04629	0.04629	0.04629	-	-	-	-
CaC <sub>2</sub> O <sub>4</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaF <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Cr(OH) <sub>3</sub>	0.04971	0.04971	0.04971	0.05453	0.05453	0.05453	0.31801	0.31801	0.31801	0.06391	0.06391	0.06391	-	-	-	-
FeOOH	0.00349	0.00349	0.00349	0.00383	0.00383	0.00383	0.02233	0.02233	0.02233	0.00449	0.00449	0.00449	-	-	-	-
Gibbsite	0.56534	0.56534	0.56534	0.62023	0.62023	0.62023	3.61681	3.61681	3.61681	0.72687	0.72687	0.72687	-	-	-	-
HgO	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
KAlSiO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
La(OH) <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
LaPO <sub>4</sub> ·2H <sub>2</sub> O	0.00042	0.00042	0.00042	0.00046	0.00046	0.00046	0.00269	0.00269	0.00269	0.00054	0.00054	0.00054	-	-	-	-
Mn(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
MnCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	0.00143	0.00143	0.00143	0.00157	0.00157	0.00157	0.00917	0.00917	0.00917	0.00184	0.00184	0.00184	-	-	-	-
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaAlSiO <sub>4</sub>	0.00011	0.00011	0.00011	0.00013	0.00013	0.00013	0.00073	0.00073	0.00073	0.00015	0.00015	0.00015	-	-	-	-
Ni(OH) <sub>2</sub>	0.00103	0.00103	0.00103	0.00113	0.00113	0.00113	0.00659	0.00659	0.00659	0.00132	0.00132	0.00132	-	-	-	-
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NiC <sub>2</sub> O <sub>4</sub> ·2H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pb(OH) <sub>2</sub>	0.00090	0.00090	0.00090	0.00098	0.00098	0.00098	0.00574	0.00574	0.00574	0.00115	0.00115	0.00115	-	-	-	-
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
PbCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pu(OH) <sub>4</sub>	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00001	0.00001	0.00001	0.00000	0.00000	0.00000	-	-	-	-
SiO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
SrCO <sub>3</sub>	0.00024	0.00024	0.00024	0.00026	0.00026	0.00026	0.00153	0.00153	0.00153	0.00031	0.00031	0.00031	-	-	-	-
TcO <sub>2</sub>	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00005	0.00005	0.00005	0.00001	0.00001	0.00001	-	-	-	-
ZrO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
KNO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	0.32204	0.32204	0.32204	-	-	-	-	-	-	0.41405	0.41405	0.41405	-	-	-	-
Na <sub>2</sub> CO <sub>3</sub> ·H <sub>2</sub> O	2.98997	2.98997	2.98997	-	-	-	-	-	-	3.84425	3.84425	3.84425	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> FSO <sub>4</sub>	0.30222	0.30222	0.30222	-	-	-	-	-	-	0.38856	0.38856	0.38856	-	-	-	-
Na <sub>3</sub> NO <sub>3</sub> SO <sub>4</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> ·8H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>4</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF(PO <sub>3</sub> ) <sub>2</sub> ·19H <sub>2</sub> O	0.53076	0.53076	0.53076	-	-	-	-	-	-	0.68240	0.68240	0.68240	-	-	-	-
NaHCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>3</sub>	3.36854	3.36854	3.36854	-	-	-	-	-	-	4.33098	4.33098	4.33098	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> ·0.25NaOH·12H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Total Volume % UDS	8.17	8.17	8.17	0.72	0.72	0.72	4.22	4.22	4.22	10.51	10.51	10.51	-	-	-	-
Solids Concentration (g/L)	186.0	186.0	186.0	19.5	19.5	19.5	114.0	114.0	114.0	239.2	239.2	239.2	-	-	-	-

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Rheological Data**

Model/model Parameter	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105
Temperature (°C)	25	45	65	25	45	65	25	45	65	25	45	65	25	45	65
Source of Data	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0
Notes	Page A29	Page A37	Page A43	Page A6	Page A15	Page A22	Page A50	Page A57	Page A64	Page A71	Page A78	Page A85	Table 2.3	Table 2.3	Table 2.3
<b>Newtonian:</b>															
$\eta$ - Newtonian viscosity (cP)	19.428	10.006	6.436	6.000	3.643	2.543	7.145	3.857	2.652	50.878	23.851	15.785	12.300	6.300	3.500
r - correlation coefficient	1.000	1.000	0.998	1.000	0.997	0.994	0.997	0.991	0.994	0.994	0.999	0.997			
<b>Ostwald (or Power Law):</b>															
m - the consistency coefficient (Pas <sup>n</sup> )	0.020	0.017	0.011	0.006	0.006	0.003	0.009	0.004	0.003	0.068	0.057	0.065			
n - the power-law exponent	0.996	0.899	0.895	0.995	0.907	1.000	0.961	1.000	0.953	0.947	0.841	0.742			
r - correlation coefficient	1.000	0.998	0.992	1.000	0.996	0.994	0.998	0.991	0.994	0.996	0.996	0.994			
<b>Bingham Plastic:</b>															
$\tau_B$ - the Bingham yield stress (Pa)	0.000	0.000	0.000	0.000	0.002	0.000	0.000	0.000	0.000	0.000	0.543	0.581	0.000	0.000	0.000
$\eta_p$ - the plastic viscosity (Pas)	0.019	0.010	0.006	0.006	0.004	0.003	0.007	0.004	0.003	0.051	0.022	0.013	<i>0.012</i>	<i>0.006</i>	<i>0.004</i>
r - correlation coefficient	1.000	1.000	0.998	1.000	0.997	0.994	0.997	0.991	0.994	0.994	0.999	0.997			
<b>Herschel-Bulkley:</b>															
$\tau_B$ - the yield stress (Pa)	0.028	0.028	0.041	0.000	0.000	0.000	0.035	0.028	0.017	0.025	0.512	0.496			
k - the Herschel-Bulkely consistency coefficient (Pa·s <sup>n</sup> )	0.020	0.017	0.010	0.006	0.006	0.003	0.007	0.004	0.003	0.051	0.026	0.025			
b - the Herschel-Bulkely power-law exponent	0.997	0.905	0.912	1.000	0.913	1.000	0.990	1.000	0.993	0.998	0.966	0.888			
r - correlation coefficient	1.000	0.998	0.993	1.000	0.996	0.994	0.997	0.991	0.994	0.994	1.000	1.000			
n/a = not applicable															

**Physical Property Data**

Physical Property	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105
Notes															
Temperature (°C)	25	45	65	25	45	65	25	45	65	25	45	65	25	45	65
Zeta Potential (mV)															
Bulk Density (g/mL)	1.49	1.49	1.49	1.33	1.33	1.33	1.34	1.34	1.34	1.51	1.51	1.51	<i>1.42</i>	<i>1.42</i>	<i>1.42</i>
vol% Settled Solids	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
Density of Centrifuged Solids (g/mL)	1.63	1.63	1.63	1.49	1.49	1.49	1.44	1.44	1.44	1.79	1.79	1.79	<i>0</i>	<i>0</i>	<i>0</i>
vol% Centrifuged Solids	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	0	0	0
wt% Centrifuged Solids	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
Supernatant Density (g/mL)	1.42	1.42	1.42	1.32	1.32	1.32	1.28	1.28	1.28	1.42	1.42	1.42	1.42	1.42	1.42
Density of Settled Solids (g/mL)	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% Settled Supernatant	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% dissolved solids in supernatant	<i>47.85</i>	<i>47.85</i>	<i>47.85</i>	<i>44.48</i>	<i>44.48</i>	<i>44.48</i>	<i>43.13</i>	<i>43.13</i>	<i>43.13</i>	<i>47.85</i>	<i>47.85</i>	<i>47.85</i>	<i>47.85</i>	<i>47.85</i>	<i>47.85</i>
wt% total solids in Centrifuged Sludge	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% Total Solids	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% UDS	<i>12.49</i>	<i>12.49</i>	<i>12.49</i>	<i>1.47</i>	<i>1.47</i>	<i>1.47</i>	<i>8.50</i>	<i>8.50</i>	<i>8.50</i>	<i>15.84</i>	<i>15.84</i>	<i>15.84</i>	0	0	0
Density of Solids (g/cc)	2.28	2.28	2.28	2.70	2.70	2.70	2.70	2.70	2.70	2.28	2.28	2.28	2.28	2.28	2.28

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Settling Data**

Settling Schedule		AN-105			AN-105		AN-105			AN-105				
Notes:		from Table 3-1c; times are estimates			from Table 3-1c; times are estimates		actually 75% dilution from Table 3-3c; times are estimates			from Table 3-3c; times are estimates				
Temperature (°C)		45			45		25			25				
Total initial volume		20			29.2		25			25				
5 minutes														
10 minutes														
15 minutes														
20 minutes														
30 minutes														
40 minutes														
50 minutes														
1 hour														
2 hours														
3 hours		15			7									
4 hours														
5 hours														
6 hours		17.5												
24 hours		11			3.5		4.5			12				
32 hours														
48 hours														
56 hours														
72 hours final settled							3.5			10.5				

**Shear Strength Data**

Shear Strength Schedule														
Source of Data														
Notes:														
Temperature (°C)														
Description														
Gelation Time/Shear Strength (Pa)														
5 minutes														
10 minutes														
15 minutes														
20 minutes														
30 minutes														
40 minutes														
50 minutes														
1 hour														
2 hours														
3 hours														
4 hours														
5 hours														
6 hours														
24 hours														
32 hours														
48 hours														
56 hours														
72 hours														
Infinite time (GRE)														

Model Chemical Data Fro

Analyte/Sample	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105
Description	dilution by volume	dilution by volume	dilution by volume	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ
Model Basis	Salt Free	Salt Free	Salt Free	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty
Report No./Source of Data	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296
Solid Phases (vol% of bulk)																
(NaAlO <sub>2</sub> ) <sub>2</sub> ·2.5H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Bi <sub>2</sub> O <sub>3</sub>	-	-	-	0.00077	0.00077	0.00077	0.00077	0.00077	0.00077	0.00077	0.00077	0.00077	0.00077	0.00077	0.00077	0.00077
BiOCl	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Boehmite	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca <sub>3</sub> (OH)(PO <sub>4</sub> ) <sub>3</sub>	-	-	-	0.08743	0.08743	0.08743	0.08743	0.08743	0.08743	0.08743	0.08743	0.08743	0.08743	0.08743	0.08743	0.08743
CaC <sub>2</sub> O <sub>4</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaF <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CrOOH	-	-	-	0.12072	0.12072	0.12072	0.12072	0.12072	0.12072	0.12072	0.12072	0.12072	0.12072	0.12072	0.12072	0.12072
FeOOH	-	-	-	0.00848	0.00848	0.00848	0.00848	0.00848	0.00848	0.00848	0.00848	0.00848	0.00848	0.00848	0.00848	0.00848
Gibbsite	-	-	-	1.37297	1.37297	1.37297	1.37297	1.37297	1.37297	1.37297	1.37297	1.37297	1.37297	1.37297	1.37297	1.37297
HgO	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
KAlSiO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
La(OH) <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
LaPO <sub>4</sub> ·2H <sub>2</sub> O	-	-	-	0.00102	0.00102	0.00102	0.00102	0.00102	0.00102	0.00102	0.00102	0.00102	0.00102	0.00102	0.00102	0.00102
Mn(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
MnCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	-	-	-	0.00348	0.00348	0.00348	0.00348	0.00348	0.00348	0.00348	0.00348	0.00348	0.00348	0.00348	0.00348	0.00348
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaAlSiO <sub>4</sub>	-	-	-	0.00028	0.00028	0.00028	0.00028	0.00028	0.00028	0.00028	0.00028	0.00028	0.00028	0.00028	0.00028	0.00028
Ni(OH) <sub>2</sub>	-	-	-	0.00250	0.00250	0.00250	0.00250	0.00250	0.00250	0.00250	0.00250	0.00250	0.00250	0.00250	0.00250	0.00250
Ni <sub>2</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NiC <sub>2</sub> O <sub>4</sub> ·2H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pb(OH) <sub>2</sub>	-	-	-	0.00218	0.00218	0.00218	0.00218	0.00218	0.00218	0.00218	0.00218	0.00218	0.00218	0.00218	0.00218	0.00218
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
PbCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pu(OH) <sub>4</sub>	-	-	-	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
SiO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
SrCO <sub>3</sub>	-	-	-	0.00058	0.00058	0.00058	0.00058	0.00058	0.00058	0.00058	0.00058	0.00058	0.00058	0.00058	0.00058	0.00058
TcO <sub>2</sub>	-	-	-	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002
ZrO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
KNO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	-	-	-	0.78210	0.78210	0.78210	0.78210	0.78210	0.78210	0.78210	0.78210	0.78210	0.78210	0.78210	0.78210	0.78210
Na <sub>2</sub> CO <sub>3</sub> ·H <sub>2</sub> O	-	-	-	7.26135	7.26135	7.26135	7.26135	7.26135	7.26135	7.26135	7.26135	7.26135	7.26135	7.26135	7.26135	7.26135
Na <sub>2</sub> SO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> FSO <sub>4</sub>	-	-	-	0.73395	0.73395	0.73395	0.73395	0.73395	0.73395	0.73395	0.73395	0.73395	0.73395	0.73395	0.73395	0.73395
Na <sub>2</sub> NO <sub>3</sub> SO <sub>4</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> ·8H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>6</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF(PO <sub>3</sub> ) <sub>2</sub> ·19H <sub>2</sub> O	-	-	-	1.28899	1.28899	1.28899	1.28899	1.28899	1.28899	1.28899	1.28899	1.28899	1.28899	1.28899	1.28899	1.28899
NaHCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>3</sub>	-	-	-	8.18075	8.18075	8.18075	8.18075	8.18075	8.18075	8.18075	8.18075	8.18075	8.18075	8.18075	8.18075	8.18075
Na <sub>3</sub> PO <sub>4</sub> ·0.25NaOH·12H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Total Volume % UDS	-	-	-	19.85	19.85	19.85	19.85	19.85	19.85	19.85	19.85	19.85	19.85	19.85	19.85	19.85
Solids Concentration (g/L)	-	-	-	451.8	451.8	451.8	451.8	451.8	451.8	451.8	451.8	451.8	451.8	451.8	451.8	451.8

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Rheological Data**

Model/model Parameter	AN-105	AN-105	AN-105													
Temperature (°C)	25	45	65													
Source of Data	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0	HNF-SD-WM-DTR-046 rev 0													
Notes	Table 2.3	Table 2.3	Table 2.3													
<b>Newtonian:</b>																
$\eta$ - Newtonian viscosity (cP)	9.400	4.200	2.400													
r - correlation coefficient																
<b>Ostwald (or Power Law):</b>																
m - the consistency coefficient (Pa·s <sup>n</sup> )																
n - the power-law exponent																
r - correlation coefficient																
<b>Bingham Plastic:</b>																
$\tau_B$ - the Bingham yield stress (Pa)	0.000	0.000	0.000													
$\eta_p$ - the plastic viscosity (Pa·s)	0.009	0.004	0.002													
r - correlation coefficient																
<b>Herschel-Bulkley:</b>																
$\tau_{Hf}$ - the yield stress (Pa)																
k - the Herschel-Bulkely consistency coefficient (Pa·s <sup>b</sup> )																
b - the Herschel-Bulkely power-law exponent																
r - correlation coefficient																
n/a = not applicable																

**Physical Property Data**

Physical Property	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105	AN-105
Notes																
Temperature (°C)	25	45	65													
Zeta Potential (mV)																
Bulk Density (g/mL)	1.35	1.35	1.35	1.59	1.59	1.59	1.59	1.59	1.59	1.59	1.59	1.59	1.59	1.59	1.59	1.59
vol% Settled Solids	n/m	n/m	n/m													
Density of Centrifuged Solids (g/mL)	0	0	0	1.66	1.66	1.66	1.66	1.66	1.66	1.66	1.66	1.66	1.66	1.66	1.66	1.66
vol% Centrifuged Solids	0	0	0													
wt% Centrifuged Solids	n/m	n/m	n/m													
Supernatant Density (g/mL)	1.35	1.35	1.35	1.42	1.42	1.42	1.42	1.42	1.42	1.42	1.42	1.42	1.42	1.42	1.42	1.42
Density of Settled Solids (g/mL)	n/m	n/m	n/m													
wt% Settled Supernatant	n/m	n/m	n/m													
wt% dissolved solids in supernatant	45.49	45.49	45.49	50	50	50	50	50	50	50	50	50	50	50	50	50
wt% total solids in Centrifuged Sludge	n/m	n/m	n/m	59	59	59	59	59	59	59	59	59	59	59	59	59
wt% Total Solids	n/m	n/m	n/m													
wt% UDS	0	0	0	28.42	28.42	28.42	28.42	28.42	28.42	28.42	28.42	28.42	28.42	28.42	28.42	28.42
Density of Solids (g/cc)	2.70	2.70	2.70	2.28	2.28	2.28	2.28	2.28	2.28	2.28	2.28	2.28	2.28	2.28	2.28	2.28





## Model Chemical Data From ESP

Analyte\Sample	AN-107	AN-107
Description	as received	as received
Model Basis	Salty	Salty
Report No./Source of Data	WSRC-TR-2003-00210, REV 0	WSRC-TR-2003-00210, REV 0
<b>Solid Phases (vol% of bulk)</b>		
(NaAlO <sub>2</sub> ) <sub>2</sub> •2.5H <sub>2</sub> O	-	-
Ag <sub>2</sub> CO <sub>3</sub>	<i>0.00000</i>	<i>0.00000</i>
Bi <sub>2</sub> O <sub>3</sub>	<i>0.00001</i>	<i>0.00001</i>
BiOCl	-	-
Boehmite	-	-
Ca(OH) <sub>2</sub>	-	-
Ca <sub>3</sub> OH(PO <sub>4</sub> ) <sub>3</sub>	-	-
CaC <sub>2</sub> O <sub>4</sub> •H <sub>2</sub> O	-	-
CaCO <sub>3</sub>	-	-
CaF <sub>2</sub>	<i>0.00359</i>	<i>0.00359</i>
CrOOH	<i>0.00051</i>	<i>0.00051</i>
FeOOH	<i>0.01104</i>	<i>0.01104</i>
Gibbsite	-	-
HgO	-	-
KAlSiO <sub>4</sub>	-	-
La(OH) <sub>3</sub>	-	-
LaPO <sub>4</sub> •2H <sub>2</sub> O	<i>0.00011</i>	<i>0.00011</i>
Mn(OH) <sub>2</sub>	-	-
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-
MnCO <sub>3</sub>	<i>0.00406</i>	<i>0.00406</i>
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	-	-
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	<i>0.16510</i>	<i>0.16510</i>
NaAlSiO <sub>4</sub>	-	-
Ni(OH) <sub>2</sub>	<i>0.00197</i>	<i>0.00197</i>
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-
NiC <sub>2</sub> O <sub>4</sub> •2H <sub>2</sub> O	-	-
Pb(OH) <sub>2</sub>	<i>0.00062</i>	<i>0.00062</i>
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-
PbCO <sub>3</sub>	-	-
Pu(OH) <sub>4</sub>	<i>0.00000</i>	<i>0.00000</i>
SiO <sub>2</sub>	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-
SrCO <sub>3</sub>	<i>0.00002</i>	<i>0.00002</i>
TcO <sub>2</sub>	<i>0.00000</i>	<i>0.00000</i>
ZrO <sub>2</sub>	<i>0.00023</i>	<i>0.00023</i>
KNO <sub>3</sub>	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	-	-
Na <sub>2</sub> CO <sub>3</sub> •H <sub>2</sub> O	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-
Na <sub>2</sub> SO <sub>4</sub> •10H <sub>2</sub> O	-	-
Na <sub>3</sub> FSO <sub>4</sub>	<i>0.04934</i>	<i>0.04934</i>
Na <sub>3</sub> NO <sub>3</sub> SO <sub>4</sub> •H <sub>2</sub> O	-	-
Na <sub>3</sub> PO <sub>4</sub> •8H <sub>2</sub> O	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> •10H <sub>2</sub> O	-	-
Na <sub>6</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-
NaF	<i>0.02402</i>	<i>0.02402</i>
NaF(PO <sub>4</sub> ) <sub>2</sub> •19H <sub>2</sub> O	-	-
NaHCO <sub>3</sub>	-	-
NaNO <sub>2</sub>	-	-
NaNO <sub>3</sub>	-	-
Na <sub>3</sub> PO <sub>4</sub> •0.25NaOH•12H <sub>2</sub> O	-	-
Total Volume % UDS	<i>0.26</i>	<i>0.26</i>
Solids Concentration (g/L)	<b>6.9</b>	<b>6.9</b>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Rheological Data**

Model/model Parameter	AN-107	AN-107
Temperature (°C)	25	40
Source of Data	WSRC-TR-2003-00210, REV 0	WSRC-TR-2003-00210, REV 0
Notes		
<b>Newtonian:</b>		
$\eta$ – Newtonian viscosity (cP)	n/m	n/m
r – correlation coefficient	n/m	n/m
<b>Ostwald (or Power Law):</b>		
m – the consistency coefficient (Pa·s <sup>-n</sup> )	n/m	n/m
n – the power-law exponent	n/m	n/m
r – correlation coefficient	n/m	n/m
<b>Bingham Plastic:</b>		
$\tau_B$ - the Bingham yield stress (Pa)	1.48	1.07
$\eta_p$ - the plastic viscosity (Pa·s)	0.00936	0.00587
r – correlation coefficient	0.997	0.993
<b>Herschel-Bulkley:</b>		
$\tau_H$ - the yield stress (Pa)	n/m	n/m
k - the Herschel-Bulkely consistency coefficient (Pa·s <sup>-b</sup> )	n/m	n/m
b - the Herschel-Bulkely power-law exponent	n/m	n/m
r – correlation coefficient	n/m	n/m
n/a = not applicable		

**Physical Property Data**

Physical Property	AN-107	AN-107
Notes		
Temperature (°C)	25	40
Zeta Potential (mV)		
Bulk Density (g/mL)	1.42	<i>1.42</i>
vol% Settled Solids	n/m	n/m
Density of Centrifuged Solids (g/mL)	<i>1.48</i>	<i>1.46</i>
vol% Centrifuged Solids	8	8
wt% Centrifuged Solids	6.88	6.88
Supernatant Density (g/mL)	1.42	<i>1.42</i>
Density of Settled Solids (g/mL)	n/m	n/m
wt% Settled Supernatant	n/m	n/m
wt% dissolved solids in supernatant	49.25	49.25
wt% total solids in Centrifuged Sludge	n/m	n/m
wt% Total Solids	49.5	49.5
wt% UDS	0.483	0.483
Density of Solids (g/cc)	<i>2.63</i>	<i>2.63</i>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

## Model Chemical Data From ESP

Analyte\Sample	AP-104	AP-104
Description	as received	as received
Model Basis	Salty	Salty
Report No./Source of Data	WTP-RPT-069, Rev. 0 (PNWD-3334)	WTP-RPT-069, Rev. 0 (PNWD-3334)
<b>Solid Phases (vol% of bulk)</b>		
(NaAlO <sub>2</sub> ) <sub>2</sub> •2.5H <sub>2</sub> O	-	-
Ag <sub>2</sub> CO <sub>3</sub>	-	-
Bi <sub>2</sub> O <sub>3</sub>	-	-
BiOCl	-	-
Boehmite	-	-
Ca(OH) <sub>2</sub>	-	-
Ca <sub>5</sub> OH(PO <sub>4</sub> ) <sub>3</sub>	-	-
CaC <sub>2</sub> O <sub>4</sub> •H <sub>2</sub> O	-	-
CaCO <sub>3</sub>	-	-
CaF <sub>2</sub>	-	-
CrOOH	-	-
FeOOH	-	-
Gibbsite	-	-
HgO	-	-
KAlSiO <sub>4</sub>	-	-
La(OH) <sub>3</sub>	-	-
LaPO <sub>4</sub> •2H <sub>2</sub> O	-	-
Mn(OH) <sub>2</sub>	-	-
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-
MnCO <sub>3</sub>	-	-
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	-	-
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	-	-
NaAlSiO <sub>4</sub>	-	-
Ni(OH) <sub>2</sub>	-	-
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-
NiC <sub>2</sub> O <sub>4</sub> •2H <sub>2</sub> O	-	-
Pb(OH) <sub>2</sub>	-	-
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-
PbCO <sub>3</sub>	-	-
Pu(OH) <sub>4</sub>	-	-
SiO <sub>2</sub>	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-
SrCO <sub>3</sub>	-	-
TcO <sub>2</sub>	-	-
ZrO <sub>2</sub>	-	-
KNO <sub>3</sub>	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	-	-
Na <sub>2</sub> CO <sub>3</sub> •H <sub>2</sub> O	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-
Na <sub>2</sub> SO <sub>4</sub> •10H <sub>2</sub> O	-	-
Na <sub>3</sub> FSO <sub>4</sub>	-	-
Na <sub>3</sub> NO <sub>3</sub> SO <sub>4</sub> •H <sub>2</sub> O	-	-
Na <sub>3</sub> PO <sub>4</sub> •8H <sub>2</sub> O	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> •10H <sub>2</sub> O	-	-
Na <sub>6</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-
NaF	-	-
NaF(PO <sub>4</sub> ) <sub>2</sub> •19H <sub>2</sub> O	-	-
NaHCO <sub>3</sub>	-	-
NaNO <sub>2</sub>	-	-
NaNO <sub>3</sub>	-	-
Na <sub>3</sub> PO <sub>4</sub> •0.25NaOH•12H <sub>2</sub> O	-	-
Total Volume % UDS	-	-
Solids Concentration (g/L)	-	-

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Rheological Data**

Model/model Parameter	AP-104	AP-104
Temperature (°C)	25	40
Source of Data	WTP-RPT-069, Rev. 0 (PNWD-3334)	WTP-RPT-069, Rev. 0 (PNWD-3334)
Notes		
<b>Newtonian:</b>		
$\eta$ – Newtonian viscosity (cP)	3.68	2.37
r – correlation coefficient	0.9982	0.9976
<b>Ostwald (or Power Law):</b>		
m – the consistency coefficient (Pa·s <sup>-n</sup> )	0.0048	0.00324
n – the power-law exponent	0.959	0.9525
r – correlation coefficient	0.999	0.9988
<b>Bingham Plastic:</b>		
$\tau_B$ - the Bingham yield stress (Pa)	0.049	0.03798
$\eta_p$ - the plastic viscosity (Pa·s)	0.0036	0.00231
r – correlation coefficient	0.9988	0.9984
<b>Herschel-Bulkley:</b>		
$\tau_H$ - the yield stress (Pa)	0	0
k - the Herschel-Bulkely consistency coefficient (Pa·s <sup>-b</sup> )	0.0048	0.00299
b - the Hershel-Bulkely power-law exponent	0.959	0.9635
r – correlation coefficient	0.999	0.9986
n/a = not applicable		

**Physical Property Data**

Physical Property	AP-104	AP-104
Notes		
Temperature (°C)	25	40
Zeta Potential (mV)		
Bulk Density (g/mL)	1.26	<i>1.26</i>
vol% Settled Solids	n/m	n/m
Density of Centrifuged Solids (g/mL)	n/m	n/m
vol% Centrifuged Solids	n/m	n/m
wt% Centrifuged Solids	n/m	n/m
Supernatant Density (g/mL)	1.30	1.30
Density of Settled Solids (g/mL)	n/m	n/m
wt% Settled Supernatant	n/m	n/m
wt% dissolved solids in supernatant	32	32
wt% total solids in Centrifuged Sludge	n/m	n/m
wt% Total Solids	31.2	31.2
wt% UDS	0.00	0.00
Density of Solids (g/cc)	<i>2.30</i>	<i>2.30</i>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

Model Chemical Data From ESP

Analyte/Sample	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101
Description	Undiluted Supernate Liquid	Undiluted Supernate Liquid	Undiluted Supernate Liquid	Undiluted Settled Solids Salty	Undiluted Settled Solids Salty	Undiluted Settled Solids Salty	Settled Solids 80% Dilution Salt Free	Settled Solids 80% Dilution Salt Free	Settled Solids 80% Dilution Salt Free	Settled Solids 80% Dilution Supernate Salt Free	Settled Solids 80% Dilution Supernate Salt Free	Settled Solids 80% Dilution Supernate Salt Free	Undiluted WTC Salty	Undiluted WTC Salty	Undiluted WTC Salty
Model Basis	Salty	Salty	Salty	Salty	Salty	Salty	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free	Salty	Salty	Salty
Report No./Source of Data	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0
<b>Solid Phases (vol% of bulk)</b>															
(NaAlO <sub>2</sub> ) <sub>2</sub> •2.5H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Bi <sub>2</sub> O <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
BiOCl	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Boehmite	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca <sub>2</sub> OH(PO <sub>4</sub> ) <sub>3</sub>	-	-	-	0.00784	0.00784	0.00784	0.12755	0.12755	0.12755	-	-	-	0.00328	0.00328	0.00328
CaC <sub>2</sub> O <sub>4</sub> •H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaF <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CrOOH	-	-	-	0.00306	0.00306	0.00306	0.04987	0.04987	0.04987	-	-	-	0.00128	0.00128	0.00128
FeOOH	-	-	-	0.00384	0.00384	0.00384	0.06250	0.06250	0.06250	-	-	-	0.00161	0.00161	0.00161
Gibbsite	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
HgO	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
KAlSiO <sub>4</sub>	-	-	-	0.02348	0.02348	0.02348	0.38204	0.38204	0.38204	-	-	-	0.00983	0.00983	0.00983
La(OH) <sub>3</sub>	-	-	-	0.00018	0.00018	0.00018	0.00286	0.00286	0.00286	-	-	-	0.00007	0.00007	0.00007
LaPO <sub>4</sub> •2H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Mn(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
MnCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	-	-	-	0.00797	0.00797	0.00797	0.12961	0.12961	0.12961	-	-	-	0.00333	0.00333	0.00333
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaAlSiO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ni(OH) <sub>2</sub>	-	-	-	0.00026	0.00026	0.00026	0.00425	0.00425	0.00425	-	-	-	0.00011	0.00011	0.00011
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NiC <sub>2</sub> O <sub>4</sub> •2H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pb(OH) <sub>2</sub>	-	-	-	0.00134	0.00134	0.00134	0.02172	0.02172	0.02172	-	-	-	0.00056	0.00056	0.00056
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
PbCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pu(OH) <sub>4</sub>	-	-	-	0.00000	0.00000	0.00000	0.00007	0.00007	0.00007	-	-	-	0.00000	0.00000	0.00000
SiO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
SrCO <sub>3</sub>	-	-	-	0.00003	0.00003	0.00003	0.00055	0.00055	0.00055	-	-	-	0.00001	0.00001	0.00001
TcO <sub>2</sub>	-	-	-	0.00001	0.00001	0.00001	0.00023	0.00023	0.00023	-	-	-	0.00001	0.00001	0.00001
ZrO <sub>2</sub>	-	-	-	0.00031	0.00031	0.00031	0.00512	0.00512	0.00512	-	-	-	0.00013	0.00013	0.00013
KNO <sub>3</sub>	-	-	-	0.60022	0.60022	0.60022	-	-	-	-	-	-	0.25127	0.25127	0.25127
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	-	-	-	0.30316	0.30316	0.30316	-	-	-	-	-	-	0.12691	0.12691	0.12691
Na <sub>2</sub> CO <sub>3</sub> •H <sub>2</sub> O	-	-	-	0.79453	0.79453	0.79453	-	-	-	-	-	-	0.33262	0.33262	0.33262
Na <sub>2</sub> SO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub> •10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> FSO <sub>4</sub>	-	-	-	0.10121	0.10121	0.10121	-	-	-	-	-	-	0.04237	0.04237	0.04237
Na <sub>3</sub> NO <sub>2</sub> SO <sub>4</sub> •H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> •8H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> •10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>6</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF(PO <sub>3</sub> ) <sub>2</sub> •19H <sub>2</sub> O	-	-	-	0.19217	0.19217	0.19217	-	-	-	-	-	-	0.08045	0.08045	0.08045
NaHCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>2</sub>	-	-	-	0.36468	0.36468	0.36468	-	-	-	-	-	-	0.15267	0.15267	0.15267
NaNO <sub>3</sub>	-	-	-	3.16232	3.16232	3.16232	-	-	-	-	-	-	1.32385	1.32385	1.32385
Na <sub>3</sub> PO <sub>4</sub> •0.25NaOH•12H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Total Volume % UDS	-	-	-	5.57	5.57	5.57	0.79	0.79	0.79	-	-	-	2.33	2.33	2.33
Solids Concentration (g/L)	-	-	-	124.8	124.8	124.8	28.8	28.8	28.8	-	-	-	52.3	52.3	52.3

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Rheological Data**

Model/model Parameter	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101
Temperature (°C)	25	45	65	25	45	65	25	45	65	25	45	65	25	45	65
Source of Data	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0
Notes	Page A-5	Page A-10	Page A-15	Not Measured Exceeded Haake CV20/ME45 Limits	Not Measured Exceeded Haake CV20/ME45 Limits	Not Measured Exceeded Haake CV20/ME45 Limits	Page A-20	Page A-25	Page A-30	Page A-35	Page A-41	Page B85	Page A-46	Page A-52	Page A-58
<b>Newtonian:</b>															
$\eta$ – Newtonian viscosity (cP)	22.000	7.992	5.357				5.357	2.822	1.750	6.000	3.010	1.800	47.142	17.478	11.210
r – correlation coefficient	1.000	1.000	0.999				0.999	0.998	0.996	1.000	1.000		0.999	0.998	0.995
<b>Ostwald (or Power Law):</b>															
m – the consistency coefficient (Pa·s <sup>n</sup> )	0.022	0.021	0.005				0.005	0.003	0.002	0.006	0.006		0.065	0.063	0.036
n – the power-law exponent	1.000	0.824	1.000				1.000	1.000	1.000	1.000	0.884		0.942	0.768	0.787
r – correlation coefficient	1.000	0.993	0.999				0.999	0.998	0.996	1.000	1.000		1.000	0.995	0.996
<b>Bingham Plastic:</b>															
$\tau_{0B}$ – the Bingham yield stress (Pa)	0.000	0.000	0.000				0.000	0.000	0.000	0.012	0.012	0.000	0.150	0.148	0.181
$\eta_p$ – the plastic viscosity (Pa·s)	0.022	0.008	0.005				0.005	0.003	0.002	0.006	0.003	<b>0.002</b>	0.047	0.017	0.010
r – correlation coefficient	1.000	1.000	0.999				0.999	0.998	0.996	1.000	1.000		0.999	0.998	0.995
<b>Herschel-Bulkley:</b>															
$\tau_{0H}$ – the yield stress (Pa)	0.000	0.000	0.000				0.000	0.000	0.000	0.012	0.011		0.006	0.006	0.006
k – the Herschel-Bulkley consistency coefficient (Pa·s <sup>b</sup> )	0.022	0.021	0.005				0.005	0.003	0.002	0.006	0.006		0.065	0.062	0.036
b – the Herschel-Bulkley power-law exponent	1.000	0.824	1.000				1.000	1.000	1.000	1.000	0.885		0.942	0.769	0.789
r – correlation coefficient	1.000	0.993	0.999				0.999	0.998	0.996	1.000	1.000		1.000	0.995	0.996
n/a = not applicable															

**Physical Property Data**

Physical Property	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101
Notes															
Temperature (°C)	25	45	65	25	45	65	25	45	65	25	45	65	25	45	65
Zeta Potential (mV)															
Bulk Density (g/mL)	1.52	1.52	1.52	1.56	1.56	1.56	1.44	1.44	1.44	1.42	1.42	1.42	1.54	1.54	1.54
vol% Settled Solids	0	0	0	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
Density of Centrifuged Solids (g/mL)	n/a	n/a	n/a	1.68	1.68	1.68	1.42	1.42	1.42	1.42	1.42	1.42	1.68	1.68	1.68
vol% Centrifuged Solids	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% Centrifuged Solids	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
Supernatant Density (g/mL)	1.52	1.52	1.52	1.52	1.52	1.52	1.42	1.42	1.42	1.42	1.42	1.42	1.52	1.52	1.52
Density of Settled Solids (g/mL)	n/a	n/a	n/a	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% Settled Supernatant	n/a	n/a	n/a	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% dissolved solids in supernatant	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% total solids in Centrifuged Sludge	n/a	n/a	n/a	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% Total Solids	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% UDS	0.00	0.00	0.00	8.00	8.00	8.00	2.00	2.00	2.00	0.00	0.00	0.00	3.40	3.40	3.40
Density of Solids (g/cc)	2.24	2.24	2.24	2.24	2.24	2.24	3.66	3.66	3.66	3.66	3.66	3.66	2.24	2.24	2.24

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Shear Strength Data**

Shear Strength Schedule															
Source of Data															
Notes:															
Temperature (°C)															
Description															
Gelation Time/Shear Strength (Pa)															
5 minutes															
10 minutes															
15 minutes															
20 minutes															
30 minutes															
40 minutes															
50 minutes															
1 hour															
2 hours															
3 hours															
4 hours															
5 hours															
6 hours															
24 hours															
32 hours															
48 hours															
56 hours															
72 hours															
Infinte time (GRE)															

Model Chemical Data Fro

Analyte/Sample	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101
Description	Diluted WTC (50% by volume)	Diluted WTC (50% by volume)	Diluted WTC (50% by volume)	Diluted WTC (50% by volume) Supernate	Diluted WTC (50% by volume) Supernate	Diluted WTC (50% by volume) Supernate	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ
Model Basis	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free	in-situ Salty	in-situ Salty	in-situ Salty	in-situ Salty	in-situ Salty	in-situ Salty	in-situ Salty	in-situ Salty
Report No./Source of Data	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296
Solid Phases (vol% of bulk)														
(NaAlO <sub>2</sub> ) <sub>2</sub> •2.5H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Bi <sub>2</sub> O <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
BiOCl	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Boehmite	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca <sub>5</sub> (OH)(PO <sub>4</sub> ) <sub>3</sub>	0.06160	0.06160	0.06160	-	-	-	0.00713	0.00713	0.00713	0.00713	0.00713	0.00713	0.00713	0.00713
CaC <sub>2</sub> O <sub>4</sub> •H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaF <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Cr(OH) <sub>3</sub>	0.02409	0.02409	0.02409	-	-	-	0.00279	0.00279	0.00279	0.00279	0.00279	0.00279	0.00279	0.00279
FeOOH	0.03019	0.03019	0.03019	-	-	-	0.00349	0.00349	0.00349	0.00349	0.00349	0.00349	0.00349	0.00349
Gibbsite	-	-	-	-	-	-	-	-	-	-	-	-	-	-
HgO	-	-	-	-	-	-	-	-	-	-	-	-	-	-
KAlSiO <sub>4</sub>	0.18451	0.18451	0.18451	-	-	-	0.02136	0.02136	0.02136	0.02136	0.02136	0.02136	0.02136	0.02136
La(OH) <sub>3</sub>	0.00138	0.00138	0.00138	-	-	-	0.00016	0.00016	0.00016	0.00016	0.00016	0.00016	0.00016	0.00016
LaPO <sub>4</sub> •2H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Mn(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
MnCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	0.06260	0.06260	0.06260	-	-	-	0.00725	0.00725	0.00725	0.00725	0.00725	0.00725	0.00725	0.00725
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaAlSiO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ni(OH) <sub>2</sub>	0.00205	0.00205	0.00205	-	-	-	0.00024	0.00024	0.00024	0.00024	0.00024	0.00024	0.00024	0.00024
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NiC <sub>2</sub> O <sub>4</sub> •2H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pb(OH) <sub>2</sub>	0.01049	0.01049	0.01049	-	-	-	0.00121	0.00121	0.00121	0.00121	0.00121	0.00121	0.00121	0.00121
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
PbCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pu(OH) <sub>4</sub>	0.00004	0.00004	0.00004	-	-	-	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
SiO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
SrCO <sub>3</sub>	0.00027	0.00027	0.00027	-	-	-	0.00003	0.00003	0.00003	0.00003	0.00003	0.00003	0.00003	0.00003
TcO <sub>2</sub>	0.00011	0.00011	0.00011	-	-	-	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001
ZrO <sub>2</sub>	0.00247	0.00247	0.00247	-	-	-	0.00029	0.00029	0.00029	0.00029	0.00029	0.00029	0.00029	0.00029
KNO <sub>3</sub>	-	-	-	-	-	-	0.54600	0.54600	0.54600	0.54600	0.54600	0.54600	0.54600	0.54600
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	-	-	-	-	-	-	0.27577	0.27577	0.27577	0.27577	0.27577	0.27577	0.27577	0.27577
Na <sub>2</sub> CO <sub>3</sub> •H <sub>2</sub> O	-	-	-	-	-	-	0.72276	0.72276	0.72276	0.72276	0.72276	0.72276	0.72276	0.72276
Na <sub>2</sub> SO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub> •10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> FSO <sub>4</sub>	-	-	-	-	-	-	0.09207	0.09207	0.09207	0.09207	0.09207	0.09207	0.09207	0.09207
Na <sub>3</sub> NO <sub>3</sub> SO <sub>3</sub> •H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> •8H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> •10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>6</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF(PO <sub>3</sub> ) <sub>2</sub> •19H <sub>2</sub> O	-	-	-	-	-	-	0.17481	0.17481	0.17481	0.17481	0.17481	0.17481	0.17481	0.17481
NaHCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>2</sub>	-	-	-	-	-	-	0.33174	0.33174	0.33174	0.33174	0.33174	0.33174	0.33174	0.33174
NaNO <sub>3</sub>	-	-	-	-	-	-	2.87665	2.87665	2.87665	2.87665	2.87665	2.87665	2.87665	2.87665
Na <sub>3</sub> PO <sub>4</sub> •0.25NaOH•12H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Total Volume % UDS	0.38	0.38	0.38	-	-	-	5.06	5.06	5.06	5.06	5.06	5.06	5.06	5.06
Solids Concentration (g/L)	13.9	13.9	13.9	-	-	-	113.5	113.5	113.5	113.5	113.5	113.5	113.5	113.5

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.



**Rheological Data**

Model/model Parameter	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101								
Temperature (°C)	25	45	65	25	45	65								
Source of Data	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	HNF-4964 Rev. 0	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296
Notes	Page A-64	Page A-69	Page A-74	Page A-79	Page A-84	Page A-89								
<b>Newtonian:</b>														
$\eta$ - Newtonian viscosity (cP)	8.286	4.214	2.571	11.500	5.351	3.641								
r - correlation coefficient	0.998	0.997	1.000	0.998	0.999	0.995								
<b>Ostwald (or Power Law):</b>														
m - the consistency coefficient (Pa·s <sup>-n</sup> )	0.010	0.004	0.003	0.011	0.006	0.006								
n - the power-law exponent	0.970	1.000	1.000	1.000	0.989	0.923								
r - correlation coefficient	0.998	0.997	1.000	0.998	0.999	0.989								
<b>Bingham Plastic:</b>														
$\tau_B$ - the Bingham yield stress (Pa)	0.020	0.000	0.000	0.000	0.000	0.085								
$\eta_p$ - the plastic viscosity (Pa·s)	0.008	0.004	0.003	0.011	0.005	0.003								
r - correlation coefficient	0.998	0.997	1.000	0.998	0.999	0.995								
<b>Herschel-Bulkley:</b>														
$\tau_H$ - the yield stress (Pa)	0.010	0.000	0.000	0.000	0.000	0.068								
k - the Herschel-Bulkely consistency coefficient (Pa·s <sup>b</sup> )	0.009	0.004	0.003	0.012	0.005	0.005								
b - the Herschel-Bulkely power-law exponent	0.977	1.000	1.000	1.000	0.999	0.917								
r - correlation coefficient	0.998	0.997	1.000	0.998	0.999	0.989								
n/a = not applicable														

**Physical Property Data**

Physical Property	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101								
Notes														
Temperature (°C)	25	45	65	25	45	65								
Zeta Potential (mV)														
Bulk Density (g/mL)	1.39	1.39	1.39	1.38	1.38	1.38	1.52	1.52	1.52	1.52	1.52	1.52	1.52	1.52
vol% Settled Solids	n/m	n/m	n/m	n/m	n/m	n/m	32.2	32.2	32.2	32.2	32.2	32.2	32.2	32.2
Density of Centrifuged Solids (g/mL)	1.006	1.006	1.006	1.006	1.006	1.006	1.68	1.68	1.68	1.68	1.68	1.68	1.68	1.68
vol% Centrifuged Solids	n/m	n/m	n/m	n/m	n/m	n/m	15.3	15.3	15.3	15.3	15.3	15.3	15.3	15.3
wt% Centrifuged Solids	n/m	n/m	n/m	n/m	n/m	n/m	16.9	16.9	16.9	16.9	16.9	16.9	16.9	16.9
Supernatant Density (g/mL)	1.38	1.38	1.38	1.38	1.38	1.38	1.52	1.52	1.52	1.52	1.52	1.52	1.52	1.52
Density of Settled Solids (g/mL)	n/m	n/m	n/m	n/m	n/m	n/m								
wt% Settled Supernatant	n/m	n/m	n/m	n/m	n/m	n/m								
wt% dissolved solids in supernatant	n/m	n/m	n/m	n/m	n/m	n/m	55	55	55	55	55	55	55	55
wt% total solids in Centrifuged Sludge	n/m	n/m	n/m	n/m	n/m	n/m	64	64	64	64	64	64	64	64
wt% Total Solids	n/m	n/m	n/m	n/m	n/m	n/m								
wt% UDS	1.00	1.00	1.00	0.00	0.00	0.00	7.47	7.47	7.47	7.47	7.47	7.47	7.47	7.47
Density of Solids (g/cc)	3.66	3.66	3.66	3.66	3.66	3.66	2.24	2.24	2.24	2.24	2.24	2.24	2.24	2.24

**Shear Strength Data**

Shear Strength Schedule							AW-101	AW-101	AW-101	AW-101	AW-101	AW-101	AW-101
Source of Data							RPP-6655	RPP-6655	RPP-6655	RPP-6655	RPP-6655	RPP-6655	RPP-6655
Notes:							Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer
Temperature (°C)							44	43	41	43	44	43	41
Description							Riser 1C Depth from bottom of tank is 200 cm	Riser 1C Depth from bottom of tank is 150 cm	Riser 1C Depth from bottom of tank is 100 cm	Riser 13A Depth from bottom of tank is 250 cm	Riser 13A Depth from bottom of tank is 200 cm	Riser 13A Depth from bottom of tank is 150 cm	Riser 13A Depth from bottom of tank is 100 cm
Gelation Time/Shear Strength (Pa)													
5 minutes													
10 minutes													
15 minutes													
20 minutes													
30 minutes													
40 minutes													
50 minutes													
1 hour													
2 hours													
3 hours													
4 hours													
5 hours													
6 hours													
24 hours													
32 hours													
48 hours													
56 hours													
72 hours													
Infinte time (GRE)							140	230	300	47	95	140	175

Model Chemical Data From ESP

Analyte/Sample	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102
Description	as received	as received	Centrifuged Liquid Composite	Centrifuged Liquid Composite	Centrifuged Liquid Composite	Retrieval Composite	Retrieval Composite	Retrieval Composite	1:1 Dilution Retrieval Composite: Centrifuged Liquid	1:1 Dilution Retrieval Composite: Centrifuged Liquid	1:1 Dilution Retrieval Composite: Centrifuged Liquid	101 g UDS/L	101 g UDS/L	101 g UDS/L	210 g UDS/L	210 g UDS/L	210 g UDS/L
Model Basis	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty
Report No./Source of Data	WSRC-TR-2003-00205, REVISION 0	WSRC-TR-2003-00205, REVISION 0	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909
Solid Phases (vol% of bulk)																	
(NaAlO <sub>2</sub> ) <sub>2</sub> ·2.5H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	0.00015	0.00015	-	-	-	0.00055	0.00055	0.00055	0.00015	0.00015	0.00015	0.00021	0.00021	0.00021	0.00044	0.00044	0.00044
B <sub>2</sub> O <sub>3</sub>	0.00042	0.00042	-	-	-	0.00155	0.00155	0.00155	0.00043	0.00043	0.00043	0.00061	0.00061	0.00061	0.00126	0.00126	0.00126
BiOCl	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Boehmite	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca <sub>2</sub> OH(PO <sub>4</sub> ) <sub>3</sub>	0.09201	0.09201	-	-	-	0.33793	0.33793	0.33793	0.09355	0.09355	0.09355	0.13246	0.13246	0.13246	0.27434	0.27434	0.27434
CaC <sub>2</sub> O <sub>4</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaF <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Cr(OH) <sub>3</sub>	0.01154	0.01154	-	-	-	0.04237	0.04237	0.04237	0.01173	0.01173	0.01173	0.01661	0.01661	0.01661	0.03440	0.03440	0.03440
FeOOH	0.80797	0.80797	-	-	-	2.96734	2.96734	2.96734	0.82144	0.82144	0.82144	1.16315	1.16315	1.16315	2.40895	2.40895	2.40895
Gibbsite	0.91660	0.91660	-	-	-	3.36630	3.36630	3.36630	0.93188	0.93188	0.93188	1.31954	1.31954	1.31954	2.73283	2.73283	2.73283
HgO	0.00003	0.00003	-	-	-	0.00010	0.00010	0.00010	0.00003	0.00003	0.00003	0.00004	0.00004	0.00004	0.00008	0.00008	0.00008
KAlSiO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
La(OH) <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
LaPO <sub>4</sub> ·2H <sub>2</sub> O	0.00832	0.00832	-	-	-	0.03057	0.03057	0.03057	0.00846	0.00846	0.00846	0.01198	0.01198	0.01198	0.02481	0.02481	0.02481
Mn(OH) <sub>2</sub>	0.14201	0.14201	-	-	-	0.52153	0.52153	0.52153	0.14437	0.14437	0.14437	0.20443	0.20443	0.20443	0.42339	0.42339	0.42339
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
MnCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	0.01765	0.01765	-	-	-	0.06482	0.06482	0.06482	0.01794	0.01794	0.01794	0.02541	0.02541	0.02541	0.05262	0.05262	0.05262
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaAlSiO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ni(OH) <sub>2</sub>	0.02024	0.02024	-	-	-	0.07432	0.07432	0.07432	0.02057	0.02057	0.02057	0.02913	0.02913	0.02913	0.06033	0.06033	0.06033
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NiC <sub>2</sub> O <sub>4</sub> ·2H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pb(OH) <sub>2</sub>	0.01344	0.01344	-	-	-	0.04934	0.04934	0.04934	0.01366	0.01366	0.01366	0.01934	0.01934	0.01934	0.04006	0.04006	0.04006
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
PbCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pu(OH) <sub>4</sub>	0.00015	0.00015	-	-	-	0.00055	0.00055	0.00055	0.00015	0.00015	0.00015	0.00021	0.00021	0.00021	0.00044	0.00044	0.00044
SiO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
SiCO <sub>3</sub>	0.00277	0.00277	-	-	-	0.01016	0.01016	0.01016	0.00281	0.00281	0.00281	0.00398	0.00398	0.00398	0.00825	0.00825	0.00825
TcO <sub>2</sub>	0.00000	0.00000	-	-	-	0.00001	0.00001	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00001	0.00001	0.00001
ZrO <sub>2</sub>	0.00011	0.00011	-	-	-	0.00041	0.00041	0.00041	0.00011	0.00011	0.00011	0.00016	0.00016	0.00016	0.00034	0.00034	0.00034
KNO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	0.08262	0.08262	-	-	-	0.30343	0.30343	0.30343	0.08400	0.08400	0.08400	0.11894	0.11894	0.11894	0.24633	0.24633	0.24633
Na <sub>2</sub> CO <sub>3</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> PSO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> NO <sub>3</sub> SO <sub>4</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> ·8H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> P <sub>2</sub> O <sub>7</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>6</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF(PO <sub>3</sub> ) <sub>2</sub> ·19H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaHCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> ·0.25NaOH·12H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Total Volume % UDS	2.12	2.12	-	-	-	7.77	7.77	7.77	2.15	2.15	2.15	3.05	3.05	3.05	6.31	6.31	6.31
Solids Concentration (g/L)	70.2	70.2	-	-	-	257.8	257.8	257.8	71.4	71.4	71.4	101.1	101.1	101.1	209.3	209.3	209.3

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

Rheological Data

Model/model Parameter	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102
Temperature (°C)	25	40	27	45	65	27	45	65	27	45	65	27	45	65	27	45	65
Source of Data	WSRC-TR-2003-00205, REVISION 0	WSRC-TR-2003-00205, REVISION 0	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909
Notes			Haake RV30 M5 Head MV-1 Sensor	Haake RV30 M5 Head MV-1 Sensor	Haake RV30 M5 Head MV-1 Sensor	Haake RV30 M5 Head MV-1 Sensor	Haake RV30 M5 Head MV-1 Sensor	Haake RV30 M5 Head MV-1 Sensor	Haake RV30 M5 Head MV-1 Sensor	Haake RV30 M5 Head MV-1 Sensor	Haake RV30 M5 Head MV-1 Sensor	Haake RV30 M5 Head MV-1 Sensor	Haake RV30 M5 Head MV-1 Sensor	Haake RV30 M5 Head MV-1 Sensor	Haake RV30 M5 Head MV-1 Sensor	Haake RV30 M5 Head MV-1 Sensor	Haake RV30 M5 Head MV-1 Sensor
<b>Newtonian:</b>																	
$\eta$ - Newtonian viscosity (cP)	4.55	3.16	1.78	1.12	0.32	3.01	1.73	0.89	2.29	0.93	1.06	2.05	1.19	1.29	3.64	2.66	1.73
$r$ - correlation coefficient	n/m	n/m															
<b>Ostwald (or Power Law):</b>																	
$m$ - the consistency coefficient (Pas <sup><i>n</i></sup> )	n/m	n/m	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a
$n$ - the power-law exponent	n/m	n/m	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a
$r$ - correlation coefficient	n/m	n/m	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a
<b>Bingham Plastic:</b>																	
$\tau_B$ - the Bingham yield stress (Pa)	1.48	1.39	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
$\eta_p$ - the plastic viscosity (Pas)	0.0043	0.0031	<i>0.00178</i>	<i>0.00112</i>	<i>0.00032</i>	<i>0.00301</i>	<i>0.00173</i>	<i>0.00089</i>	<i>0.00229</i>	<i>0.00093</i>	<i>0.00106</i>	<i>0.00205</i>	<i>0.00119</i>	<i>0.00129</i>	<i>0.00364</i>	<i>0.00266</i>	<i>0.00173</i>
$r$ - correlation coefficient	n/m	n/m	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a
<b>Herschel-Bulkley:</b>																	
$\tau_H$ - the yield stress (Pa)	n/m	n/m	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a
$k$ - the Herschel-Bulkley consistency coefficient (Pas <sup><i>b</i></sup> )	n/m	n/m	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a
$b$ - the Herschel-Bulkley power-law exponent	n/m	n/m	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a
$r$ - correlation coefficient	n/m	n/m	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a
n/a = not applicable																	

Physical Property Data

Physical Property	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102	AY-102
Notes			RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909	RPP-8909
Temperature (°C)	25	40	Ambient	Ambient	Ambient	Ambient	Ambient	Ambient	Ambient	Ambient	Ambient	Ambient	Ambient	Ambient	Ambient	Ambient	Ambient
Zeta Potential (mV)																	
Bulk Density (g/mL)	1.2	<i>1.2</i>	<i>1.13</i>	<i>1.13</i>	<i>1.13</i>	1.3	1.3	1.3	1.17	1.17	1.17	1.24	1.24	1.24	1.3	1.3	1.3
vol% Settled Solids	n/m	n/m	0	0	0	52	52	52									
Density of Centrifuged Solids (g/mL)	1.37	1.37	n/m	n/m	n/m	n/m	n/m	n/m									
vol% Centrifuged Solids	18	18	0	0	0	40	40	40									
wt% Centrifuged Solids	20.4	20.4	0	0	0												
Supernatant Density (g/mL)	1.15	1.15	1.13	1.13	1.13	1.13	1.13	1.13	1.13	1.13	1.13	1.13	1.13	1.13	1.13	1.13	1.13
Density of Settled Solids (g/mL)	n/m	n/m	n/m	n/m	n/m	1.47	1.47	1.47									
wt% Settled Supernatant	n/m	n/m	100	100	100	41	41	41									
wt% dissolved solids in supernatant	16.3	16.3	15.5	15.5	15.5	16	16	16									
wt% total solids in Centrifuged Sludge	45.5	45.5	n/m	n/m	n/m	46	46	46									
wt% Total Solids	21.2	21.2	15.5	15.5	15.5												
wt% UDS	5.85	5.85	<i>0.00</i>	<i>0.00</i>	<i>0.00</i>	<i>19.83</i>	<i>19.83</i>	<i>19.83</i>	6.10	6.10	6.10	8.15	8.15	8.15	16.10	16.10	16.10
Density of Solids (g/cc)	3.32	3.32	3.32	3.32	3.32	3.32	3.32	3.32	3.32	3.32	3.32	3.32	3.32	3.32	3.32	3.32	3.32

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Settling Data**

Settling Schedule						AY-102 RPP-8909 No Temp. Mentioned	AY-102 RPP-8909 No Temp. Mentioned	AY-102 RPP-8909 No Temp. Mentioned										
Notes:						Ambient	Ambient	Ambient										
Temperature (°C)						Ambient	Ambient	Ambient										
Total initial volume						94	94	94										
5 minutes																		
10 minutes																		
15 minutes						93.5	93.5	93.5										
20 minutes																		
30 minutes						93	93	93										
40 minutes																		
50 minutes																		
1 hour						91	91	91										
2 hours						88	88	88										
3 hours						81.5	81.5	81.5										
4 hours						80	80	80										
5 hours						77	77	77										
6 hours						75.5	75.5	75.5										
24 hours						62.5	62.5	62.5										
32 hours																		
48 hours						55.5	55.5	55.5										
56 hours																		
72 hours final settled						52	52	52										

**Shear Strength Data**

Shear Strength Schedule	AY-102	AY-102																
Source of Data	WSRC-TR-2003-00205, REVISION 0	WSRC-TR-2003-00205, REVISION 0																
Notes:	Haake RV30/MS	Haake RV30/MS																
Temperature (°C)	0	0																
Description	Sample Settled for 48 hrs prior to shear strength testing; no settled solids physical properties values are available	Sample Settled for 48 hrs prior to shear strength testing; no settled solids physical properties values are available																
Gelation Time/Shear Strength (Pa)																		
5 minutes																		
10 minutes																		
15 minutes																		
20 minutes																		
30 minutes																		
40 minutes																		
50 minutes																		
1 hour																		
2 hours																		
3 hours																		
4 hours																		
5 hours																		
6 hours																		
24 hours																		
32 hours																		
48 hours	43	0																
56 hours																		
72 hours																		
infinte time (GRE)																		

## Model Chemical Data From ESP

Analyte Sample	AZ-101	AZ-101
Description	as received	Caustic Washed and Leached
Model Basis	Salty	Leached
Report No./Source of Data	WTP-RPT-043, Rev 1	WTP-RPT-043, Rev 1
Solid Phases (vol% of bulk)		
(NaAlO <sub>2</sub> ) <sub>2</sub> ·2.5H <sub>2</sub> O	-	-
Ag <sub>2</sub> CO <sub>3</sub>	<i>0.00293</i>	<i>0.00328</i>
Bi <sub>2</sub> O <sub>3</sub>	-	-
BiOCl	-	-
Boehmite	-	-
Ca(OH) <sub>2</sub>	-	-
Ca <sub>2</sub> OH(PO <sub>4</sub> ) <sub>3</sub>	<i>0.10549</i>	<i>0.11795</i>
CaC <sub>2</sub> O <sub>4</sub> ·H <sub>2</sub> O	-	-
CaCO <sub>3</sub>	-	-
CaF <sub>2</sub>	-	-
CrOOH	<i>0.00304</i>	<i>0.00340</i>
FeOOH	<i>1.60010</i>	<i>1.78914</i>
Gibbsite	<i>5.72952</i>	-
HgO	-	-
KAlSiO <sub>4</sub>	-	-
La(OH) <sub>3</sub>	-	-
LaPO <sub>4</sub> ·2H <sub>2</sub> O	<i>0.05674</i>	<i>0.06344</i>
Mn(OH) <sub>2</sub>	<i>0.02700</i>	<i>0.03019</i>
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-
MnCO <sub>3</sub>	-	-
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	<i>0.07502</i>	<i>0.08388</i>
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	-	-
NaAlSiO <sub>4</sub>	<i>0.16550</i>	<i>0.18505</i>
Ni(OH) <sub>2</sub>	<i>0.10189</i>	<i>0.11393</i>
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-
NiC <sub>2</sub> O <sub>4</sub> ·2H <sub>2</sub> O	-	-
Pb(OH) <sub>2</sub>	<i>0.00253</i>	<i>0.00283</i>
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-
PbCO <sub>3</sub>	-	-
Pu(OH) <sub>4</sub>	<i>0.00083</i>	<i>0.00093</i>
SiO <sub>2</sub>	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-
SrCO <sub>3</sub>	<i>0.00964</i>	<i>0.01078</i>
TcO <sub>2</sub>	<i>0.00001</i>	<i>0.00001</i>
ZrO <sub>2</sub>	<i>0.36110</i>	<i>0.40376</i>
KNO <sub>3</sub>	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	-	-
Na <sub>2</sub> CO <sub>3</sub> ·H <sub>2</sub> O	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-
Na <sub>2</sub> SO <sub>4</sub> ·10H <sub>2</sub> O	-	-
Na <sub>3</sub> FSO <sub>4</sub>	-	-
Na <sub>3</sub> NO <sub>3</sub> SO <sub>4</sub> ·H <sub>2</sub> O	-	-
Na <sub>3</sub> PO <sub>4</sub> ·8H <sub>2</sub> O	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> ·10H <sub>2</sub> O	-	-
Na <sub>4</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-
NaF	-	-
NaF(PO <sub>4</sub> ) <sub>2</sub> ·19H <sub>2</sub> O	-	-
NaHCO <sub>3</sub>	-	-
NaNO <sub>2</sub>	-	-
NaNO <sub>3</sub>	-	-
Na <sub>3</sub> PO <sub>4</sub> ·0.25NaOH·12H <sub>2</sub> O	-	-
Total Volume % UDS	<i>8.24</i>	<i>2.81</i>
Solids Concentration (g/L)	<b>248.8</b>	<b>123.2</b>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Rheological Data**

Model/model Parameter	<i>AZ-101</i>	<i>AZ-101</i>
Temperature (°C)	25	25
Source of Data	<i>WTP-RPT-043, Rev 1</i>	<i>WTP-RPT-043, Rev 1</i>
Notes		
<b>Newtonian:</b>		
$\eta$ – Newtonian viscosity (cP)	n/m	n/m
r – correlation coefficient	n/m	n/m
<b>Ostwald (or Power Law):</b>		
m – the consistency coefficient (Pa·s <sup>-n</sup> )	n/m	n/m
n – the power-law exponent	n/m	n/m
r – correlation coefficient	n/m	n/m
<b>Bingham Plastic:</b>		
$\tau_B$ - the Bingham yield stress (Pa)	3.9	1.4
$\eta_p$ - the plastic viscosity (Pa·s)	0.0083	0.0029
r – correlation coefficient	0.99	0.98
<b>Herschel-Bulkley:</b>		
$\tau_H$ - the yield stress (Pa)	2.4	0.873
k - the Herschel-Bulkely consistency coefficient (Pa·s <sup>b</sup> )	0.0592	0.0346
b - the Herschel-Bulkely power-law exponent	0.5	0.5
r – correlation coefficient	1	0.98
n/a = not applicable		

**Physical Property Data**

Physical Property	<i>AZ-101</i>	<i>AZ-101</i>
Notes		
Temperature (°C)	25	25
Zeta Potential (mV)		
Bulk Density (g/mL)	1.39	1.13
vol% Settled Solids	n/m	n/m
Density of Centrifuged Solids (g/mL)	1.61	1.48
vol% Centrifuged Solids	36.4	20.5
wt% Centrifuged Solids	43.9	27
Supernatant Density (g/mL)	1.19	1
Density of Settled Solids (g/mL)	n/m	n/m
wt% Settled Supernatant	n/m	n/m
wt% dissolved solids in supernatant	26.2	3.43
wt% total solids in Centrifuged Sludge	n/m	n/m
wt% Total Solids	38.8	13.7
wt% UDS	17.90	10.90
Density of Solids (g/cc)	<i>3.02</i>	<i>4.39</i>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

## Model Chemical Data From ESP

Analyte/Sample	AZ-102	AZ-102	AZ-102
Description	as received with 6:1 wt 0.01 NaOH added	concentrated slurry as received with 6:1 wt 0.01 NaOH added	Caustic Washed and Leached
Model Basis	Salt Free	Salt Free	Leached
Report No./Source of Data	BNFL-RPT-038 Rev. 0	BNFL-RPT-038 Rev. 0	BNFL-RPT-038 Rev. 0
<b>Solid Phases (vol% of bulk)</b>			
(NaAlO <sub>2</sub> ) <sub>2</sub> •2.5H <sub>2</sub> O	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	<i>0.00207</i>	<i>0.00571</i>	<i>0.00532</i>
Bi <sub>2</sub> O <sub>3</sub>	<i>0.00013</i>	<i>0.00035</i>	<i>0.00033</i>
BiOCl	-	-	-
Boehmite	-	-	-
Ca(OH) <sub>2</sub>	-	-	-
Ca <sub>2</sub> OH(PO <sub>4</sub> ) <sub>3</sub>	<i>0.02282</i>	<i>0.06286</i>	<i>0.05856</i>
CaC <sub>2</sub> O <sub>4</sub> •H <sub>2</sub> O	-	-	-
CaCO <sub>3</sub>	-	-	-
CaF <sub>2</sub>	-	-	-
CrOOH	<i>0.00304</i>	<i>0.00838</i>	<i>0.00781</i>
FeOOH	<i>0.36541</i>	<i>1.00640</i>	<i>0.93763</i>
Gibbsite	<i>0.66849</i>	<i>1.84113</i>	-
HgO	-	-	-
KAlSiO <sub>4</sub>	-	-	-
La(OH) <sub>3</sub>	-	-	-
LaPO <sub>4</sub> •2H <sub>2</sub> O	<i>0.00933</i>	<i>0.02569</i>	<i>0.02394</i>
Mn(OH) <sub>2</sub>	<i>0.01000</i>	<i>0.02753</i>	<i>0.02565</i>
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-
MnCO <sub>3</sub>	-	-	-
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	<i>0.02076</i>	<i>0.05718</i>	<i>0.05328</i>
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	<i>0.48125</i>	<i>1.32544</i>	<i>1.23487</i>
NaAlSiO <sub>4</sub>	<i>0.16669</i>	<i>0.45908</i>	<i>0.42771</i>
Ni(OH) <sub>2</sub>	<i>0.02233</i>	<i>0.06150</i>	<i>0.05730</i>
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-
NiC <sub>2</sub> O <sub>4</sub> •2H <sub>2</sub> O	-	-	-
Pb(OH) <sub>2</sub>	<i>0.00184</i>	<i>0.00508</i>	<i>0.00473</i>
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-
PbCO <sub>3</sub>	-	-	-
Pu(OH) <sub>4</sub>	<i>0.00023</i>	<i>0.00063</i>	<i>0.00059</i>
SiO <sub>2</sub>	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-
SrCO <sub>3</sub>	<i>0.00097</i>	<i>0.00267</i>	<i>0.00249</i>
TcO <sub>2</sub>	<i>0.00001</i>	<i>0.00002</i>	<i>0.00002</i>
ZrO <sub>2</sub>	<i>0.03346</i>	<i>0.09216</i>	<i>0.08586</i>
KNO <sub>3</sub>	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	-	-	-
Na <sub>2</sub> CO <sub>3</sub> •H <sub>2</sub> O	-	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-	-
Na <sub>2</sub> SO <sub>4</sub> •10H <sub>2</sub> O	-	-	-
Na <sub>3</sub> FSO <sub>4</sub>	-	-	-
Na <sub>3</sub> NO <sub>3</sub> SO <sub>4</sub> •H <sub>2</sub> O	-	-	-
Na <sub>3</sub> PO <sub>4</sub> •8H <sub>2</sub> O	-	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> •10H <sub>2</sub> O	-	-	-
Na <sub>6</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-	-
NaF	-	-	-
NaF(PO <sub>4</sub> ) <sub>2</sub> •19H <sub>2</sub> O	-	-	-
NaHCO <sub>3</sub>	-	-	-
NaNO <sub>2</sub>	-	-	-
NaNO <sub>3</sub>	-	-	-
Na <sub>3</sub> PO <sub>4</sub> •0.25NaOH•12H <sub>2</sub> O	-	-	-
Total Volume % UDS	<i>1.81</i>	<i>4.98</i>	<i>2.93</i>
Solids Concentration (g/L)	<b>53.8</b>	<b>148.2</b>	<b>96.6</b>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.



**Rheological Data**

Model/model Parameter	AZ-102	AZ-102	AZ-102
Temperature (°C)	25	25	25
Source of Data	BNFL-RPT-038 Rev. 0	BNFL-RPT-038 Rev. 0	BNFL-RPT-038 Rev. 0
Notes	Appendix F; Figure 4	Appendix F; Figure 9	Appendix F; Figure 15
<b>Newtonian:</b>			
$\eta$ – Newtonian viscosity (cP)	2.589	9.908	17.74
r – correlation coefficient	0.993	0.962	0.84
<b>Ostwald (or Power Law):</b>			
m – the consistency coefficient (Pa·s <sup>-n</sup> )	0.022	0.177	2.45
n – the power-law exponent	0.631	0.504	0.25
r – correlation coefficient	0.986	0.982	0.99
<b>Bingham Plastic:</b>			
$\tau_B$ - the Bingham yield stress (Pa)	0.134	1.377	6.53
$\eta_p$ - the plastic viscosity (Pa·s)	0.002	0.006	0.01
r – correlation coefficient	0.993	0.962	0.84
<b>Herschel-Bulkley:</b>			
$\tau_H$ - the yield stress (Pa)	0.000	0.939	4.55
k - the Herschel-Bulkely consistency coefficient (Pa·s <sup>-b</sup> )	0.027	0.047	0.26
b - the Hershel-Bulkely power-law exponent	0.593	0.671	0.52
r – correlation coefficient	0.983	0.983	0.95
n/a = not applicable			

**Physical Property Data**

Physical Property	AZ-102	AZ-102	AZ-102
Notes			
Temperature (°C)	25	25	25
Zeta Potential (mV)			
Bulk Density (g/mL)	<i>1.06</i>	1.09	1.05
vol% Settled Solids	n/m	96	93
Density of Centrifuged Solids (g/mL)	n/m	1.36	1.2
	n/m	26	26
vol% Centrifuged Solids	n/m	33	30
wt% Centrifuged Solids			
Supernatant Density (g/mL)	1.02	1.02	1.04
Density of Settled Solids (g/mL)	n/m	1.07	1.07
	n/m	95	94
wt% Settled Supernatant			
wt% dissolved solids in supernatant	n/m	n/m	n/m
wt% total solids in Centrifuged Sludge	n/m	n/m	n/m
wt% Total Solids			
wt% UDS	5.10	13.60	9.20
Density of Solids (g/cc)	<i>2.98</i>	<i>2.98</i>	<i>3.30</i>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

## Model Chemical Data From ESP

Analyte\Sample	B-111	B-111
Description	no dilution	no dilution
Model Basis	Salty	Salty
Report No/Source of Data	Segment 3; WHC-SD- WM-ER-382, rev 0	Segment 5; WHC-SD- WM-ER-382, rev 0
Solid Phases (vol% of bulk)		
(NaAlO <sub>2</sub> ) <sub>2</sub> •2.5H <sub>2</sub> O	-	-
Ag <sub>2</sub> CO <sub>3</sub>	<i>0.00014</i>	<i>0.00021</i>
Bi <sub>2</sub> O <sub>3</sub>	<i>0.25830</i>	<i>0.40743</i>
BiOCl	<i>0.08115</i>	<i>0.12801</i>
Boehmite	-	-
Ca(OH) <sub>2</sub>	-	-
Ca <sub>5</sub> (OH)(PO <sub>4</sub> ) <sub>3</sub>	-	-
CaC <sub>2</sub> O <sub>4</sub> •H <sub>2</sub> O	-	-
CaCO <sub>3</sub>	-	-
CaF <sub>2</sub>	<i>0.05600</i>	<i>0.08834</i>
CrOOH	<i>0.03960</i>	<i>0.06247</i>
FeOOH	<i>0.81578</i>	<i>1.28677</i>
Gibbsite	-	-
HgO	-	-
KAlSiO <sub>4</sub>	-	-
La(OH) <sub>3</sub>	-	-
LaPO <sub>4</sub> •2H <sub>2</sub> O	<i>0.00027</i>	<i>0.00043</i>
Mn(OH) <sub>2</sub>	-	-
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-
MnCO <sub>3</sub>	<i>0.00699</i>	<i>0.01102</i>
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	-	-
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	<i>0.26333</i>	<i>0.41536</i>
NaAlSiO <sub>4</sub>	-	-
Ni(OH) <sub>2</sub>	-	-
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-
NiC <sub>2</sub> O <sub>4</sub> •2H <sub>2</sub> O	<i>0.00284</i>	<i>0.00448</i>
Pb(OH) <sub>2</sub>	-	-
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-
PbCO <sub>3</sub>	<i>0.04051</i>	<i>0.06390</i>
Pu(OH) <sub>4</sub>	<i>0.00004</i>	<i>0.00006</i>
SiO <sub>2</sub>	<i>1.02591</i>	<i>1.61821</i>
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-
SrCO <sub>3</sub>	<i>0.01394</i>	<i>0.02198</i>
TcO <sub>2</sub>	<i>0.00010</i>	<i>0.00016</i>
ZrO <sub>2</sub>	<i>0.00045</i>	<i>0.00071</i>
KNO <sub>3</sub>	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	<i>0.26828</i>	<i>0.42317</i>
Na <sub>2</sub> CO <sub>3</sub> •H <sub>2</sub> O	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-
Na <sub>2</sub> SO <sub>4</sub> •10H <sub>2</sub> O	-	-
Na <sub>2</sub> FSO <sub>4</sub>	-	-
Na <sub>3</sub> NO <sub>3</sub> SO <sub>4</sub> •H <sub>2</sub> O	-	-
Na <sub>3</sub> PO <sub>4</sub> •8H <sub>2</sub> O	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> •10H <sub>2</sub> O	<i>6.86039</i>	<i>10.82119</i>
Na <sub>6</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-
NaF	-	-
NaF(PO <sub>4</sub> ) <sub>2</sub> •19H <sub>2</sub> O	-	-
NaHCO <sub>3</sub>	-	-
NaNO <sub>2</sub>	-	-
NaNO <sub>3</sub>	-	-
Na <sub>3</sub> PO <sub>4</sub> •0.25NaOH•12H <sub>2</sub> O	-	-
Total Volume % UDS	<i>9.73</i>	<i>15.35</i>
Solids Concentration (g/L)	<b>236.2</b>	<b>372.6</b>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Physical Property Data**

Physical Property	<i>B-111</i>	<i>B-111</i>
Notes		
Temperature (°C)	<b>30</b>	<b>30</b>
Zeta Potential (mV)		
Bulk Density (g/mL)	1.27	1.35
vol% Settled Solids	100	100
Density of Centrifuged Solids (g/mL)	1.38	1.45
vol% Centrifuged Solids	57	63
wt% Centrifuged Solids	55	67
Supernatant Density (g/mL)	1.15	1.17
Density of Settled Solids (g/mL)	n/m	n/m
wt% Settled Supernatant	n/m	n/m
wt% dissolved solids in supernatant	11.60	9.60
wt% total solids in Centrifuged Sludge	n/m	n/m
wt% Total Solids	30.2	37.2
wt% UDS	18.60	27.60
Density of Solids (g/cc)	<b>2.43</b>	<b>2.43</b>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Shear Strength Data**

Shear Strength Schedule	<i>B-111</i>	<i>B-111</i>
Source of Data	<i>Segment 3; WHC-SD-WM-ER-382, rev 0</i>	<i>Segment 5; WHC-SD-WM-ER-382, rev 0</i>
Notes:	Page 5-14	Page 5-14
Temperature (°C)	Unspecified	Unspecified
Description	Shear Vane at unspecified gel time or temperature	Shear Vane at unspecified gel time or temperature
Gelation Time/Shear Strength (Pa)		
5 minutes		
10 minutes		
15 minutes		
20 minutes		
30 minutes		
40 minutes		
50 minutes		
1 hour		
2 hours		
3 hours		
4 hours		
5 hours		
6 hours		
24 hours		
32 hours		
48 hours		
56 hours		
72 hours		
Infinte time (GRE)	< 30	90

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

Model Chemical Data From ESP

Analyte/Sample	B-201	B-201	B-201	B-201	B-201	B-201	B-201	B-201	B-201	B-201	B-201	B-201	B-201	B-201	B-201
Description	as-received Segment 2	1:1 dilution by volume Segment 2 Sample 1	1:1 dilution by volume Segment 2 Sample 2	3:1 dilution by volume Segment 2 Sample 1	3:1 dilution by volume Segment 2 Sample 2	as-received Segment 5	1:1 dilution by volume Segment 5 Sample 2	1:1 dilution by volume Segment 5 Sample 3	3:1 dilution by volume Segment 5 Sample 1	3:1 dilution by volume Segment 5 Sample 2	as-received Segment 8	1:1 dilution by volume Segment 8 Sample 1	1:1 dilution by volume Segment 8 Sample 2	3:1 dilution by volume Segment 8 Sample 1	3:1 dilution by volume Segment 8 Sample 2
Model Basis	Salty	Salt Free	Salt Free	Salt Free	Salt Free	Salty	Salt Free	Salt Free	Salt Free	Salt Free	Salty	Salt Free	Salt Free	Salt Free	Salt Free
Source of Data	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037
Solid Phases (vol% of bulk)															
(NaAlO <sub>2</sub> ) <sub>2</sub> ·2.5H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	0.00049	0.00033	0.00033	0.00009	0.00010	0.00034	0.00017	0.00017	0.00005	0.00005	0.00030	0.00012	0.00012	0.00004	0.00004
Bi <sub>2</sub> O <sub>3</sub>	3.16783	2.12494	2.12494	0.59764	0.66248	2.20371	1.12621	1.12621	0.33124	0.33124	1.92925	0.79685	0.79685	0.26562	0.26562
BiOCl	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Boehmite	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca <sub>3</sub> (OH)(PO <sub>3</sub> ) <sub>3</sub>	0.12911	0.08661	0.08661	0.02436	0.02700	0.08982	0.04590	0.04590	0.01350	0.01350	0.07863	0.03248	0.03248	0.01083	0.01083
CaC <sub>2</sub> O <sub>4</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaF <sub>2</sub>	0.91939	0.61671	0.61671	0.17345	0.19227	0.63957	0.32686	0.32686	0.09613	0.09613	0.55992	0.23127	0.23127	0.07709	0.07709
CrOOH	0.23154	0.15531	0.15531	0.04368	0.04842	0.16107	0.08232	0.08232	0.02421	0.02421	0.14101	0.05824	0.05824	0.01941	0.01941
FeOOH	1.16999	0.78481	0.78481	0.22073	0.24468	0.81390	0.41595	0.41595	0.12234	0.12234	0.71254	0.29430	0.29430	0.09910	0.09910
Gibbsite	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
HgO	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
KAlSiO <sub>4</sub>	0.66521	0.44621	0.44621	0.12550	0.13911	0.46275	0.23649	0.23649	0.06956	0.06956	0.40512	0.16733	0.16733	0.05578	0.05578
La(OH) <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
LaPO <sub>4</sub> ·2H <sub>2</sub> O	1.08160	0.72552	0.72552	0.20405	0.22619	0.75242	0.38453	0.38453	0.11310	0.11310	0.65871	0.27207	0.27207	0.09069	0.09069
Mn(OH) <sub>2</sub>	1.59222	1.06804	1.06804	0.30039	0.33297	1.10763	0.56606	0.56606	0.16649	0.16649	0.96968	0.40051	0.40051	0.13350	0.13350
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	0.45470	0.30500	0.30500	0.08578	0.09509	0.31631	0.16165	0.16165	0.04754	0.04754	0.27692	0.11438	0.11438	0.03813	0.03813
MnCO <sub>3</sub>	1.67269	1.12202	1.12202	0.31557	0.34980	1.16361	0.59467	0.59467	0.17490	0.17490	1.01869	0.42076	0.42076	0.14025	0.14025
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	0.00946	0.00634	0.00634	0.00178	0.00198	0.00658	0.00336	0.00336	0.00099	0.00099	0.00576	0.00238	0.00238	0.00079	0.00079
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaAlSiO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ni(OH) <sub>2</sub>	0.04743	0.03181	0.03181	0.00895	0.00992	0.03299	0.01686	0.01686	0.00496	0.00496	0.02888	0.01193	0.01193	0.00398	0.00398
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NiC <sub>2</sub> O <sub>4</sub> ·2H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pb(OH) <sub>2</sub>	0.01233	0.00827	0.00827	0.00233	0.00258	0.00858	0.00438	0.00438	0.00129	0.00129	0.00751	0.00310	0.00310	0.00103	0.00103
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
PbCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pu(OH) <sub>4</sub>	0.00072	0.00048	0.00048	0.00014	0.00015	0.00050	0.00025	0.00025	0.00007	0.00007	0.00044	0.00018	0.00018	0.00006	0.00006
SiO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
SrCO <sub>3</sub>	0.11901	0.07983	0.07983	0.02245	0.02489	0.08279	0.04231	0.04231	0.01244	0.01244	0.07248	0.02994	0.02994	0.00998	0.00998
TcO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
ZrO <sub>2</sub>	0.00120	0.00080	0.00080	0.00023	0.00025	0.00083	0.00043	0.00043	0.00013	0.00013	0.00073	0.00030	0.00030	0.00010	0.00010
KNO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	0.28196	-	-	-	-	0.19615	-	-	-	-	0.17172	-	-	-	-
Na <sub>2</sub> CO <sub>3</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> FSO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> NO <sub>3</sub> SO <sub>3</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> ·8H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> P <sub>2</sub> O <sub>7</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> (SO <sub>4</sub> ) <sub>2</sub> ·CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF(PO <sub>3</sub> ) <sub>2</sub> ·19H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaHCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> ·0.25NaOH·12H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Total Volume % UDS	11.56	7.56	7.56	2.13	2.36	8.04	4.01	4.01	1.18	1.18	7.04	2.84	2.84	0.95	0.95
Solids Concentration (g/L)	597.5	396.4	396.4	111.5	123.6	415.7	210.1	210.1	61.8	61.8	363.9	148.6	148.6	49.5	49.5

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Rheological Data**

Model/model Parameter	B-201	B-201	B-201	B-201	B-201	B-201	B-201	B-201	B-201	B-201	B-201	B-201	B-201	B-201	B-201
Temperature (°C)	30	30	30	30	30	30	30	30	30	30	30	30	30	30	30
Source of Data	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037
Instrumentation	Haake RV100 M5 Head/Shear Vane	Haake RV100	Haake RV100	Haake RV100	Haake RV100	Haake RV100	Haake RV100	Haake RV100	Haake RV100	Haake RV100	Haake RV100	Haake RV100	Haake RV100	Haake RV100	Haake RV100
<b>Newtonian:</b>															
$\eta$ - Newtonian viscosity (cP)		n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a
r - correlation coefficient		n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a
<b>Ostwald (or Power Law):</b>															
m - the consistency coefficient (Pas <sup>-n</sup> )		n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a
n - the power-law exponent		n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a
r - correlation coefficient		n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a
<b>Bingham Plastic:</b>															
$\tau_B$ - the Bingham yield stress (Pa)		1.21	2.41	0.37	0.34		4.35	6.56	0.20	0.39		9.68	7.25	0.34	0.37
$\eta_p$ - the plastic viscosity (Pas)		0.0040	0.0050	0.0020	0.0019		0.010	0.009	0.0016	0.0017		0.012	0.012	0.0019	0.0017
r - correlation coefficient		0.98	0.98	0.99	1.00		0.91	1.00	0.97	0.99		0.99	0.99	1.00	0.98
<b>Herschel-Bulkley:</b>															
$\tau_{HP}$ - the yield stress (Pa)		1.20	2.25	n/a	n/a		2.91	6.38	n/a	n/a		9.21	6.39	n/a	n/a
k - the Herschel-Bulkely consistency coefficient (Pas <sup>n</sup> )		0.004	0.022	n/a	n/a		0.392	0.025	n/a	n/a		0.055	0.097	n/a	n/a
n - the Herschel-Bulkely power-law exponent		0.99	0.76	n/a	n/a		0.44	0.84	n/a	n/a		0.76	0.67	n/a	n/a
r - correlation coefficient		0.98	0.98	n/a	n/a		0.95	1.00	n/a	n/a		1.00	1.00	n/a	n/a
n/a = not applicable															

**Physical Property Data**

Physical Property	B-201	B-201	B-201	B-201	B-201	B-201	B-201	B-201	B-201	B-201	B-201	B-201	B-201	B-201	B-201
Source of Data	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037	PNNL-14221 WHC-SD-WM-DP-037
Temperature (°C)	30	30	30	30	30	30	30	30	30	30	30	30	30	30	30
Zeta Potential (mV)							n/m				n/m	n/m	n/m	n/m	n/m
Bulk Density (g/mL)	1.65	1.33	1.33	1.1	1.1	1.51	1.17	1.17	1.05	1.05	1.34	1.13	1.13	1.05	1.05
vol% Settled Solids	100	82.7	82.9	42.5	42.2	100	80	81.5	36.9	37.1	100	91.8	91.9	43.9	42.2
Density of Centrifuged Solids (g/mL)	1.66	1.59	1.59	1.48	1.48	1.52	1.4	1.4	1.36	1.36	1.37	1.33	1.33	1.24	1.24
vol% Centrifuged Solids	98	57.4	58.8	24	23.4	98	43.8	43.1	16.2	16.2	88	41.3	42.5	23.5	19.4
wt% Centrifuged Solids	98	67.6	69.5	32.3	31.1	98	52.1	51.5	21.3	20.2	90	49.2	48.7	25	25.1
Supernatant Density (g/mL)	1.19	1.01	1.01	1.01	1	1.19	1.00	1.00	1.00	1.00	1.05	1.01	1.01	1.01	1.01
Density of Settled Solids (g/mL)	1.65					1.51					1.34				
wt% Settled Supernatant	0					0					0				
wt% dissolved solids in supernatant	n/m					n/m					n/m				
wt% total solids in Centrifuged Sludge															
wt% Total Solids	53.6					31.6					28				
wt% UDS	36.21	29.80	29.80	10.13	11.23	27.53	17.96	17.96	5.88	5.88	27.16	13.15	13.15	4.72	4.72
Density of Solids (g/cc)	5.17	5.24	5.24	5.24	5.24	5.17	5.24	5.24	5.24	5.24	5.17	5.24	5.24	5.24	5.24

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

Shear Strength Data

Shear Strength Schedule	B-201				B-201				B-201			
Source of Data	PNNL-14221 WHC-SD-WM-DP-037				PNNL-14221 WHC-SD-WM-DP-037				PNNL-14221 WHC-SD-WM-DP-037			
Instrumentation	Haake RV100/M5 Shear Vane				Haake RV100/M5 Shear Vane				Haake RV100/M5 Shear Vane			
Temperature (°C)	30				30				30			
Description	As-Received Sample before it was disturbed. Placed in water bath at temperature for a minimum of 1 hr.				As-Received Sample before it was disturbed. Placed in water bath at temperature for a minimum of 1 hr.				As-Received Sample before it was disturbed. Placed in water bath at temperature for a minimum of 1 hr.			
Gelation Time/Shear Strength (Pa)												
5 minutes												
10 minutes												
15 minutes												
20 minutes												
30 minutes												
40 minutes												
50 minutes												
1 hour		1410				1310				1220		
2 hours												
3 hours												
4 hours												
5 hours												
6 hours												
24 hours												
32 hours												
48 hours												
56 hours												
72 hours												
Infinite time (GRE)												

## Model Chemical Data From ESP

Analyte/Sample	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	
Description	as-received Segment 2	1:1 dilution by volume Segment 2 Sample 1	1:1 dilution by volume Segment 2 Sample 2	1:1 dilution by volume Segment 2 Sample 1	1:1 dilution by volume Segment 2 Sample 2	3:1 dilution by volume Segment 2 Sample 1	3:1 dilution by volume Segment 2 Sample 2	3:1 dilution by volume Segment 2 Sample 1	3:1 dilution by volume Segment 2 Sample 2	3:1 dilution by volume Segment 2 Sample 1	3:1 dilution by volume Segment 2 Sample 2	as-received Segment 3 Core 25	as-received Segment 4 Core 24	1:1 dilution by volume Segment 4 Sample 1	1:1 dilution by volume Segment 4 Sample 2	1:1 dilution by volume Segment 4 Sample 1	1:1 dilution by volume Segment 4 Sample 2
Model Basis	Salty	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free	Salty	Salty	Salt Free	Salt Free	Salt Free	Salt Free
Source of Data	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371
Solid Phases (vol% of bulk)																	
(NaAlO <sub>2</sub> ) <sub>2</sub> ·2.5H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	0.00039	0.00010	0.00010	0.00010	0.00010	0.00004	0.00005	0.00004	0.00005	0.00004	0.00005	0.00021	0.00028	0.00011	0.00010	0.00011	0.00010
Bi <sub>2</sub> O <sub>3</sub>	1.33956	0.33534	0.33534	0.33534	0.33534	0.12648	0.17006	0.12648	0.17006	0.12648	0.17006	0.73282	0.96318	0.38898	0.34528	0.38898	0.34528
BiOCl	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Boehmite	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca <sub>3</sub> OH(PO <sub>4</sub> ) <sub>3</sub>	0.25056	0.06272	0.06272	0.06272	0.06272	0.02366	0.03181	0.02366	0.03181	0.02366	0.03181	0.13707	0.18016	0.07276	0.06458	0.07276	0.06458
CaC <sub>2</sub> O <sub>4</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaF <sub>2</sub>	1.02712	0.25712	0.25712	0.25712	0.25712	0.09698	0.13040	0.09698	0.13040	0.09698	0.13040	0.56190	0.73853	0.29825	0.26475	0.29825	0.26475
CrOOH	0.20299	0.05082	0.05082	0.05082	0.05082	0.01917	0.02577	0.01917	0.02577	0.01917	0.02577	0.11105	0.14595	0.05894	0.05232	0.05894	0.05232
FeOOH	1.39181	0.34842	0.34842	0.34842	0.34842	0.13141	0.17669	0.13141	0.17669	0.13141	0.17669	0.76140	1.00075	0.40415	0.35875	0.40415	0.35875
Gibbsite	0.40722	0.10194	0.10194	0.10194	0.10194	0.03845	0.05170	0.03845	0.05170	0.03845	0.05170	0.22277	0.29280	0.11825	0.10496	0.11825	0.10496
HgO	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
KAlSiO <sub>4</sub>	0.21924	0.05488	0.05488	0.05488	0.05488	0.02070	0.02783	0.02070	0.02783	0.02070	0.02783	0.11994	0.15764	0.06366	0.05651	0.06366	0.05651
La(OH) <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
LaPO <sub>4</sub> ·2H <sub>2</sub> O	1.11929	0.28020	0.28020	0.28020	0.28020	0.10568	0.14210	0.10568	0.14210	0.10568	0.14210	0.61232	0.80480	0.32501	0.28850	0.32501	0.28850
Mn(OH) <sub>2</sub>	1.94287	0.48637	0.48637	0.48637	0.48637	0.18345	0.24665	0.18345	0.24665	0.18345	0.24665	1.06287	1.39698	0.56416	0.50079	0.56416	0.50079
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
MnCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	0.02398	0.00600	0.00600	0.00600	0.00600	0.00226	0.00304	0.00226	0.00304	0.00226	0.00304	0.01312	0.01725	0.00696	0.00618	0.00696	0.00618
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaAlSiO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ni(OH) <sub>2</sub>	0.02496	0.00625	0.00625	0.00625	0.00625	0.00236	0.00317	0.00236	0.00317	0.00236	0.00317	0.01366	0.01795	0.00725	0.00643	0.00725	0.00643
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NiC <sub>2</sub> O <sub>4</sub> ·2H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pb(OH) <sub>2</sub>	0.03167	0.00793	0.00793	0.00793	0.00793	0.00299	0.00402	0.00299	0.00402	0.00299	0.00402	0.01732	0.02277	0.00920	0.00816	0.00920	0.00816
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
PbCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pu(OH) <sub>4</sub>	0.00014	0.00004	0.00004	0.00004	0.00004	0.00001	0.00002	0.00001	0.00002	0.00001	0.00002	0.00008	0.00010	0.00004	0.00004	0.00004	0.00004
SiO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
SrCO <sub>3</sub>	0.07431	0.01860	0.01860	0.01860	0.01860	0.00702	0.00943	0.00702	0.00943	0.00702	0.00943	0.04065	0.05343	0.02158	0.01916	0.02158	0.01916
TcO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
ZrO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
KNO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	0.57198	-	-	-	-	-	-	-	-	-	-	0.31291	0.41127	-	-	-	-
Na <sub>2</sub> CO <sub>3</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> FSO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> NO <sub>3</sub> SO <sub>4</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> ·8H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> (SO <sub>4</sub> ) <sub>2</sub> ·CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF(PO <sub>3</sub> ) <sub>2</sub> ·19H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaHCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> ·0.25NaOH·12H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Total Volume % UDS	8.63	2.02	2.02	2.02	2.02	0.76	1.02	0.76	1.02	0.76	1.02	4.72	6.20	2.34	2.08	2.34	2.08
Solids Concentration (g/L)	402.2	97.3	97.3	97.3	97.3	36.7	49.4	36.7	49.4	36.7	49.4	220.0	289.2	112.9	100.2	112.9	100.2

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.



**Rheological Data**

Model/model Parameter	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202		
Temperature (°C)		30		30		95		95		30		30		95		95		30
Source of Data	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	
Instrumentation	Haake RV100 M5 Head/Shear Vane	Haake RV100	Haake RV100	Haake RV100	Haake RV100	Haake RV100	Haake RV100	Haake RV100	Haake RV100	Haake RV100	Haake RV100 M5 Head/Shear Vane	Haake RV100 M5 Head/Shear Vane	Haake RV100	Haake RV100	Haake RV100	Haake RV100	Haake RV100	
<b>Newtonian:</b>																		
$\eta$ - Newtonian viscosity (cP)		n/a	n/a	n/a	n/a	2.20		1.50		1.20			n/a	n/a	n/a	n/a	2	
$r$ - correlation coefficient		n/a	n/a	n/a	n/a	0.99		0.75					n/a	n/a	n/a	n/a		
<b>Ostwald (or Power Law):</b>																		
$m$ - the consistency coefficient (Pas <sup>n</sup> )		n/a	n/a	n/a	n/a	n/a		n/a		n/a			n/a	n/a	n/a	n/a	n/a	
$n$ - the power-law exponent		n/a	n/a	n/a	n/a	n/a		n/a		n/a			n/a	n/a	n/a	n/a	n/a	
$r$ - correlation coefficient		n/a	n/a	n/a	n/a	n/a		n/a		n/a			n/a	n/a	n/a	n/a	n/a	
<b>Bingham Plastic:</b>																		
$\tau_B$ - the Bingham yield stress (Pa)		0.62	0.54	1.41	0.67	0.00		0.00		0.00			1.04	0.93	1.06	0.90	0.00	
$\eta_p$ - the plastic viscosity (Pas)		0.0027	0.0027	0.0026	0.0021	<b>0.0022</b>		<b>0.0015</b>		<b>0.0012</b>			0.031	0.004	0.0022	0.0017	<b>0.0020</b>	
$r$ - correlation coefficient		1.00	0.99	0.99	0.97	n/a		n/a		n/a			0.90	0.96	0.96	0.97	n/a	
<b>Herschel-Bulkley:</b>																		
$\tau_B$ - the yield stress (Pa)		1.08	0.68	2.10	1.40	n/a		n/a		n/a			1.00	1.00	1.60	1.00	n/a	
$k$ - the Herschel-Bulkley consistency coefficient (Pas <sup>b</sup> )		0.002	0.003	0.001	0.002	n/a		n/a		n/a			0.006	0.003	0.008	0.001	n/a	
$b$ - the Herschel-Bulkley power-law exponent		1.00	0.97	1.00	1.00	n/a		n/a		n/a			0.88	1.00	1.00	1.00	n/a	
$r$ - correlation coefficient						n/a		n/a		n/a							n/a	
n/a = not applicable																		

**Physical Property Data**

Physical Property	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202
Source of Data	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371
Temperature (°C)	30	30	30	95	95	30	30					30	30	30	95	95	30
Zeta Potential (mV)	n/m											n/m					
Bulk Density (g/mL)	1.23	1.10	1.10	1.10	1.10	1.04	1.05	1.04	1.05	1.23	1.2	1.11	1.10	1.11	1.10	1.04	
vol% Settled Solids	100	77	76			38	38					100	80	80		39	
Density of Centrifuged Solids (g/mL)	1.32	n/m	n/m									1.29					
vol% Centrifuged Solids	67	n/m	n/m									60.8					
wt% Centrifuged Solids	71.5	n/m	n/m									65.4					
Supernatant Density (g/mL)	1.06	1.02	1.02	1.02	1.02	1.01	1.01	1.01	1.01	1.06	1.05	1.02	1.02	1.02	1.02	1.01	
Density of Settled Solids (g/mL)	1.23	n/m	n/m														
wt% Settled Supernatant	0											0					
wt% dissolved solids in supernatant	n/m											n/m					
wt% total solids in Centrifuged Sludge																	
wt% Total Solids	36.2											28.5					
wt% UDS	32.70	8.85	8.85	8.85	8.85	3.53	4.70	3.53	4.70	17.89	24.10	10.17	9.11	10.17	9.11	3.66	
Density of Solids (g/cc)	4.66	4.83	4.83	4.83	4.83	4.83	4.83	4.83	4.83	4.66	4.66	4.83	4.83	4.83	4.83	4.83	

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Settling Data**

Settling Schedule	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202
Source of Data	WHC-SD-WM-DP-034	WHC-SD-WM-DP-034			WHC-SD-WM-DP-034	WHC-SD-WM-DP-034				WHC-SD-WM-DP-034	WHC-SD-WM-DP-034		WHC-SD-WM-DP-034
Temperature (°C)	30	30			30	30				30	30		30
Total initial volume	11.8	12.7			11.2	11				11.3	11.9		12.2
5 minutes													
10 minutes	11.8	12.7			9.7	10.2							
15 minutes										11.3	11.9		11.4
20 minutes													
30 minutes	11.8	12.7			8.4	9.2				11.3	11.9		10.3
40 minutes													
50 minutes	11.8	12.7			7.7	8.3				11.3	11.9		9.5
1 hour	11.7	12.5			7.2	7.7				11.1	11.7		9
2 hours	11.4	12.2			6	6.3				10.9	11.4		7.3
3 hours	11.1	11.8			5.4	5.5				10.4	11		6.4
4 hours	10.6	11.4			5.1	5				10.4	10.8		5.8
5 hours	10.3	11.2			5	4.9				10.3	10.6		5.6
6 hours	10.2	11			4.9	4.8				10.1	10.4		5.4
24 hours	9.4	9.9			4.5	4.5				9.2	9.7		5
32 hours	9.2	9.8			4.3	4.4				9.1	9.6		4.8
48 hours	9.1	9.7			4.2	4.3				9	9.5		4.7
56 hours	9.1	9.7			4.2	4.2				9	9.5		
72 hours final settled	9.1	9.7			4.2	4.2				9	9.5		4.7

**Shear Strength Data**

Shear Strength Schedule	B-202									B-202	B-202					
Source of Data	PNNL-14221 WHC-SD-WM-DP-034									PNNL-14221 WHC-SD-WM-DP-034	PNNL-14221 WHC-SD-WM-DP-034					
Instrumentation	Haake RV100/M5 Shear Vane									Haake RV100/M5 Shear Vane	Haake RV100/M5 Shear Vane					
Temperature (°C)	30									30	30					
Description	As-Received Sample before it was disturbed. Placed in water bath at temperature for a minimum of 1 hr.									As-Received Sample before it was disturbed. Placed in water bath at temperature for a minimum of 1 hr.	As-Received Sample before it was disturbed. Placed in water bath at temperature for a minimum of 1 hr.					
Gelation Time/Shear Strength (Pa)																
5 minutes																
10 minutes																
15 minutes																
20 minutes																
30 minutes																
40 minutes																
50 minutes																
1 hour																
2 hours																
3 hours																
4 hours																
5 hours																
6 hours																
24 hours																
32 hours																
48 hours																
56 hours																
72 hours																
Infinite time (GRE)	200									270	750					

Model Chemical Data Fro

Analyte/Sample	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202
Description	3:1 dilution by volume Segment 4 Sample 2	3:1 dilution by volume Segment 4 Sample 1	3:1 dilution by volume Segment 4 Sample 2	as-received Segment 5 Core 25	as-received Segment 6 Core 24	1:1 dilution by volume Segment 6 Sample 1	1:1 dilution by volume Segment 6 Sample 2	1:1 dilution by volume Segment 6 Sample 1	1:1 dilution by volume Segment 6 Sample 2	3:1 dilution by volume Segment 6 Sample 1	3:1 dilution by volume Segment 6 Sample 2	3:1 dilution by volume Segment 6 Sample 1	3:1 dilution by volume Segment 6 Sample 2	as-received Segment 7 Core 25
Model Basis	Salt Free	Salt Free	Salt Free	Salty	Salty	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free	Salty
Source of Data	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371	PNNL-14221 WHC-SD-WM-DP-034 WHC-SD-WM-ER-371
<b>Solid Phases (vol% of bulk)</b>														
(NaAlO <sub>2</sub> ) <sub>2</sub> ·2.5H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	0.00004	0.00004	0.00004	0.00040	0.00028	0.0010	0.0011	0.00005	0.00004	0.00005	0.00004	0.00005	0.00004	0.00042
Bi <sub>2</sub> O <sub>3</sub>	0.13123	0.13123	0.13123	1.37561	0.94703	0.33666	0.38026	0.33666	0.38026	0.15719	0.14684	0.15719	0.14684	1.45353
BiOCl	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Boehmite	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca <sub>5</sub> (OH)(PO <sub>4</sub> ) <sub>3</sub>	0.02455	0.02455	0.02455	0.25730	0.17714	0.06297	0.07113	0.06297	0.07113	0.02940	0.02747	0.02940	0.02747	0.27188
CaC <sub>2</sub> O <sub>4</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaF <sub>2</sub>	0.10062	0.10062	0.10062	1.05476	0.72615	0.25814	0.29157	0.25814	0.29157	0.12053	0.11259	0.12053	0.11259	1.11451
CrOOH	0.01989	0.01989	0.01989	0.20845	0.14351	0.05102	0.05762	0.05102	0.05762	0.02382	0.02225	0.02382	0.02225	0.22026
FeOOH	0.13634	0.13634	0.13634	1.42926	0.98397	0.34979	0.39509	0.34979	0.39509	0.16332	0.15256	0.16332	0.15256	1.51023
Gibbsite	0.03989	0.03989	0.03989	0.41818	0.28789	0.10234	0.11560	0.10234	0.11560	0.04779	0.04464	0.04779	0.04464	0.44187
HgO	-	-	-	-	-	-	-	-	-	-	-	-	-	-
KAlSiO <sub>4</sub>	0.02148	0.02148	0.02148	0.22514	0.15499	0.05510	0.06223	0.05510	0.06223	0.02573	0.02403	0.02573	0.02403	0.23789
La(OH) <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
LaPO <sub>4</sub> ·2H <sub>2</sub> O	0.10965	0.10965	0.10965	1.14940	0.79130	0.28130	0.31773	0.28130	0.31773	0.13134	0.12269	0.13134	0.12269	1.21452
Mn(OH) <sub>2</sub>	0.19033	0.19033	0.19033	1.99515	1.37355	0.48828	0.55152	0.48828	0.55152	0.22799	0.21297	0.22799	0.21297	2.10817
Mn <sub>2</sub> (PO <sub>4</sub> ) <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
MnCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	0.00235	0.00235	0.00235	0.02463	0.01696	0.00603	0.00681	0.00603	0.00681	0.00281	0.00263	0.00281	0.00263	0.02603
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaAlSiO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ni(OH) <sub>2</sub>	0.00245	0.00245	0.00245	0.02563	0.01765	0.00627	0.00709	0.00627	0.00709	0.00293	0.00274	0.00293	0.00274	0.02708
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NiC <sub>2</sub> O <sub>4</sub> ·2H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pb(OH) <sub>2</sub>	0.00310	0.00310	0.00310	0.03252	0.02239	0.00796	0.00899	0.00796	0.00899	0.00372	0.00347	0.00372	0.00347	0.03436
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
PbCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pu(OH) <sub>4</sub>	0.00001	0.00001	0.00001	0.00015	0.00010	0.00004	0.00004	0.00004	0.00004	0.00002	0.00002	0.00002	0.00002	0.00016
SiO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
SrCO <sub>3</sub>	0.00728	0.00728	0.00728	0.07631	0.05254	0.01868	0.02110	0.01868	0.02110	0.00872	0.00815	0.00872	0.00815	0.08064
TcO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
ZrO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
KNO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	-	-	-	0.58737	0.40437	-	-	-	-	-	-	-	-	0.62065
Na <sub>2</sub> CO <sub>3</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> FSO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> NO <sub>3</sub> ·SO <sub>4</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> PO <sub>4</sub> ·8H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> P <sub>2</sub> O <sub>7</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> (SO <sub>4</sub> ) <sub>2</sub> ·CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF(PO <sub>3</sub> ) <sub>2</sub> ·19H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaHCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> PO <sub>4</sub> ·0.25NaOH·12H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Total Volume % UDS	0.79	0.79	0.79	8.86	6.10	2.02	2.29	2.02	2.29	0.95	0.88	0.95	0.88	9.36
Solids Concentration (g/L)	38.1	38.1	38.1	413.0	284.4	97.7	110.4	97.7	110.4	45.6	42.6	45.6	42.6	436.4

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Rheological Data**

Model/model Parameter	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202
Temperature (°C)	30	95	95			29	29	95	95	29	29	95	95	
Source of Data	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>
Instrumentation	Haake RV100	Haake RV100	Haake RV100	Haake RV100 MS Head/Shear Vane	Haake RV100 MS Head/Shear Vane	Haake RV100	Haake RV100	Haake RV100	Haake RV100	Haake RV100	Haake RV100	Haake RV100	Haake RV100	Haake RV100 MS Head/Shear Vane
<b>Newtonian:</b>														
$\eta$ - Newtonian viscosity (cP)	2	1	2			n/a	n/a	n/a	n/a	2.00	2.00	1.00	2.00	
r - correlation coefficient						n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	
<b>Ostwald (or Power Law):</b>														
m - the consistency coefficient (Pas <sup>n</sup> )	n/a	n/a	n/a			n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	
n - the power-law exponent	n/a	n/a	n/a			n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	
r - correlation coefficient	n/a	n/a	n/a			n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	
<b>Bingham Plastic:</b>														
$\tau_B$ - the Bingham yield stress (Pa)	0.00	0.00	0.00			1.12	1.07	0.87	1.07	0.00	0.00	0.00	0.00	
$\eta_p$ - the plastic viscosity (Pas)	<i>0.0020</i>	<i>0.0010</i>	<i>0.0020</i>			0.004	0.003	0.002	0.003	<i>0.0020</i>	<i>0.0020</i>	<i>0.0010</i>	<i>0.0020</i>	
r - correlation coefficient	n/a	n/a	n/a			0.99	1.00	0.99	1.00	n/a	n/a	n/a	n/a	
<b>Herschel-Bulkley:</b>														
$\tau_0$ - the yield stress (Pa)	n/a	n/a	n/a			1.16	1.11	1.65	1.30	n/a	n/a	n/a	n/a	
k - the Herschel-Bulkely consistency coefficient (Pas <sup>n</sup> )	n/a	n/a	n/a			0.020	0.015	0.007	0.001	n/a	n/a	n/a	n/a	
b - the Herschel-Bulkely power-law exponent	n/a	n/a	n/a			0.74	0.78	1.00	1.00	n/a	n/a	n/a	n/a	
r - correlation coefficient	n/a	n/a	n/a							n/a	n/a	n/a	n/a	
n/a = not applicable														

**Physical Property Data**

Physical Property	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202	B-202
Source of Data	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>	<i>PNNL-14221</i> <i>WHC-SD-WM-DP-034</i> <i>WHC-SD-WM-ER-371</i>
Temperature (°C)	30				30	29	29	95	95	29	29	95	95	
Zeta Potential (mV)					n/m	n/m	n/m			n/m	n/m	n/m	n/m	
Bulk Density (g/mL)	1.04	1.04	1.04	1.37	1.21	1.09	1.10	1.09	1.10	<i>1.04</i>	<i>1.04</i>	<i>1.04</i>	<i>1.04</i>	1.37
vol% Settled Solids	<i>39</i>				100	<i>86</i>	<i>86</i>			<i>48</i>	<i>47</i>			
Density of Centrifuged Solids (g/mL)					1.29									
vol% Centrifuged Solids					68.8									
wt% Centrifuged Solids					73.3									
Supernatant Density (g/mL)	<i>1.01</i>	<i>1.01</i>	<i>1.01</i>	<i>1.05</i>	1.03	<i>1.01</i>	<i>1.01</i>	<i>1.01</i>	<i>1.01</i>	<i>1.01</i>	<i>1.01</i>	<i>1.01</i>	<i>1.01</i>	<i>1.03</i>
Density of Settled Solids (g/mL)					1.21									
wt% Settled Supernatant					0									
wt% dissolved solids in supernatant					n/m									
wt% total solids in Centrifuged Sludge					27									
wt% Total Solids	<i>3.66</i>	<i>3.66</i>	<i>3.66</i>	<i>30.15</i>	23.50	<i>8.97</i>	<i>10.03</i>	<i>8.97</i>	<i>10.03</i>	<i>4.38</i>	<i>4.10</i>	<i>4.38</i>	<i>4.10</i>	<i>31.86</i>
wt% UDS	<i>4.83</i>	<i>4.83</i>	<i>4.83</i>	<i>4.66</i>	<i>4.66</i>	<i>4.83</i>	<i>4.83</i>	<i>4.83</i>	<i>4.83</i>	<i>4.83</i>	<i>4.83</i>	<i>4.83</i>	<i>4.83</i>	<i>4.66</i>
Density of Solids (g/cc)														

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Settling Data**

Settling Schedule	B-202				B-202				B-202			
Source of Data	WHC-SD-WM-DP-034				WHC-SD-WM-DP-034				WHC-SD-WM-DP-034			
Temperature (°C)	30				29				29			
Total initial volume	12.2				12.4				12.2			
5 minutes												
10 minutes												
15 minutes	11.8				12.4				12.2			
20 minutes												
30 minutes	11.1				12.4				12.2			
40 minutes												
50 minutes	10.3				12.4				12.2			
1 hour	9.8				12.2				12.2			
2 hours	7.8				12				11.9			
3 hours	6.7				11.8				11.8			
4 hours	6				11.5				11.5			
5 hours	5.7				11.5				11.5			
6 hours	5.5				11.3				11.3			
24 hours	5				10.8				10.9			
32 hours	5				10.7				10.7			
48 hours	4.8				10.7				10.6			
56 hours					10.7				10.5			
72 hours final settled	4.8				10.7				10.5			

**Shear Strength Data**

Shear Strength Schedule	B-202				B-202				B-202			
Source of Data	PNNL-14221 WHC-SD-WM-DP-034				PNNL-14221 WHC-SD-WM-DP-034				PNNL-14221 WHC-SD-WM-DP-034			
Instrumentation	Haake RV100/M5 Shear Vane				Haake RV100/M5 Shear Vane				Haake RV100/M5 Shear Vane			
Temperature (°C)	30				30				30			
Description	As-Received Sample before it was disturbed. Placed in water bath at temperature for a minimum of 1 hr.				As-Received Sample before it was disturbed. Placed in water bath at temperature for a minimum of 1 hr.				As-Received Sample before it was disturbed. Placed in water bath at temperature for a minimum of 1 hr.			
Gelation Time/Shear Strength (Pa)												
5 minutes												
10 minutes												
15 minutes												
20 minutes												
30 minutes												
40 minutes												
50 minutes												
1 hour												
2 hours												
3 hours												
4 hours												
5 hours												
6 hours												
24 hours												
32 hours												
48 hours												
56 hours												
72 hours												
Infinte time (GRE)	470				750				270			

## Model Chemical Data From ESP

Analyte/Sample	B-203	B-203	B-203	B-203	B-203
Description	Homogenized Tank Composite	30 wt% dilution of a core composite	1:1 Dilution of a core composite	1:1 Dilution of a core composite	4:1 Dilution of a core composite
Model Basis	Salty	Washed	Washed	Washed	Washed
Source of Data	PNNL-14365	PNNL-14365	PNNL-14365	PNNL-14365	PNNL-14365
Solid Phases (vol% of bulk)					
(NaAlO <sub>2</sub> ) <sub>2</sub> •2.5H <sub>2</sub> O	-	-	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	<i>0.00008</i>	<i>0.00012</i>	<i>0.00009</i>	<i>0.00009</i>	<i>0.00002</i>
Bi <sub>2</sub> O <sub>3</sub>	<i>0.45700</i>	<i>0.70830</i>	<i>0.50930</i>	<i>0.50930</i>	<i>0.12562</i>
BiOCl	-	-	-	-	-
Boehmite	-	-	-	-	-
Ca(OH) <sub>2</sub>	-	-	-	-	-
Ca <sub>3</sub> OH(PO <sub>4</sub> ) <sub>3</sub>	-	-	-	-	-
CaC <sub>2</sub> O <sub>4</sub> •H <sub>2</sub> O	-	-	-	-	-
CaCO <sub>3</sub>	-	-	-	-	-
CaF <sub>2</sub>	<i>0.01200</i>	<i>0.01859</i>	<i>0.01337</i>	<i>0.01337</i>	<i>0.00330</i>
CrOOH	<i>0.08346</i>	<i>0.12935</i>	<i>0.09301</i>	<i>0.09301</i>	<i>0.02294</i>
FeOOH	<i>0.10857</i>	<i>0.16827</i>	<i>0.12100</i>	<i>0.12100</i>	<i>0.02984</i>
Gibbsite	-	-	-	-	-
HgO	-	-	-	-	-
KAlSiO <sub>4</sub>	<i>0.01013</i>	<i>0.01571</i>	<i>0.01129</i>	<i>0.01129</i>	<i>0.00279</i>
La(OH) <sub>3</sub>	<i>0.03248</i>	<i>0.05033</i>	<i>0.03619</i>	<i>0.03619</i>	<i>0.00893</i>
LaPO <sub>4</sub> •2H <sub>2</sub> O	<i>0.25651</i>	<i>0.39756</i>	<i>0.28587</i>	<i>0.28587</i>	<i>0.07051</i>
Mn(OH) <sub>2</sub>	<i>0.58814</i>	<i>0.91154</i>	<i>0.65544</i>	<i>0.65544</i>	<i>0.16167</i>
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-
MnCO <sub>3</sub>	<i>0.04020</i>	<i>0.06230</i>	<i>0.04480</i>	<i>0.04480</i>	<i>0.01105</i>
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	<i>0.00368</i>	<i>0.00570</i>	<i>0.00410</i>	<i>0.00410</i>	<i>0.00101</i>
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	-	-	-	-	-
NaAlSiO <sub>4</sub>	-	-	-	-	-
Ni(OH) <sub>2</sub>	<i>0.00620</i>	<i>0.00961</i>	<i>0.00691</i>	<i>0.00691</i>	<i>0.00170</i>
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-
NiC <sub>2</sub> O <sub>4</sub> •2H <sub>2</sub> O	-	-	-	-	-
Pb(OH) <sub>2</sub>	<i>0.00331</i>	<i>0.00513</i>	<i>0.00369</i>	<i>0.00369</i>	<i>0.00091</i>
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-
PbCO <sub>3</sub>	-	-	-	-	-
Pu(OH) <sub>4</sub>	<i>0.00006</i>	<i>0.00009</i>	<i>0.00007</i>	<i>0.00007</i>	<i>0.00002</i>
SiO <sub>2</sub>	-	-	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-
SrCO <sub>3</sub>	<i>0.02107</i>	<i>0.03266</i>	<i>0.02348</i>	<i>0.02348</i>	<i>0.00579</i>
TcO <sub>2</sub>	<i>0.00000</i>	<i>0.00000</i>	<i>0.00000</i>	<i>0.00000</i>	<i>0.00000</i>
ZrO <sub>2</sub>	<i>0.00006</i>	<i>0.00009</i>	<i>0.00006</i>	<i>0.00006</i>	<i>0.00002</i>
KNO <sub>3</sub>	-	-	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	-	-	-	-	-
Na <sub>2</sub> CO <sub>3</sub> •H <sub>2</sub> O	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub> •10H <sub>2</sub> O	-	-	-	-	-
Na <sub>2</sub> FSO <sub>4</sub>	-	-	-	-	-
Na <sub>2</sub> NO <sub>3</sub> SO <sub>4</sub> •H <sub>2</sub> O	-	-	-	-	-
Na <sub>2</sub> PO <sub>4</sub> •8H <sub>2</sub> O	-	-	-	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> •10H <sub>2</sub> O	-	-	-	-	-
Na <sub>6</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-
NaF	-	-	-	-	-
NaF(PO <sub>4</sub> ) <sub>2</sub> •19H <sub>2</sub> O	-	-	-	-	-
NaHCO <sub>3</sub>	-	-	-	-	-
NaNO <sub>2</sub>	-	-	-	-	-
NaNO <sub>3</sub>	-	-	-	-	-
Na <sub>2</sub> PO <sub>4</sub> •0.25NaOH•12H <sub>2</sub> O	-	-	-	-	-
Total Volume % UDS	<i>1.62</i>	<i>2.52</i>	<i>1.81</i>	<i>1.81</i>	<i>0.45</i>
Solids Concentration (g/L)	<b>89.6</b>	<b>138.9</b>	<b>99.9</b>	<b>99.9</b>	<b>24.6</b>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

## Rheological Data

Model/model Parameter		B-203	B-203	B-203	B-203
Temperature (°C)		25	25	25	25
Source of Data	<i>PNNL-14365</i>	<i>PNNL-14365</i>	<i>PNNL-14365</i>	<i>PNNL-14365</i>	<i>PNNL-14365</i>
Instrumentation		Haake RS300 Concentric Cylinders with a 3 mm Gap	Haake RS300 Concentric Cylinders with a 3 mm Gap	Haake RS300 Concentric Cylinders with a 3 mm Gap	Haake RS300 Concentric Cylinders with a 3 mm Gap
<b>Newtonian:</b>					
$\eta$ – Newtonian viscosity (cP)		n/a	n/a	n/a	n/a
r – correlation coefficient		n/a	n/a	n/a	n/a
<b>Ostwald (or Power Law):</b>					
m – the consistency coefficient (Pa·s <sup>-n</sup> )		n/a	n/a	n/a	n/a
n – the power-law exponent		n/a	n/a	n/a	n/a
r – correlation coefficient		n/a	n/a	n/a	n/a
<b>Bingham Plastic:</b>					
$\tau_B$ - the Bingham yield stress (Pa)		10.90	3.07	3.15	0.13
$\eta_p$ - the plastic viscosity (Pa·s)		0.0079	0.0047	0.0047	0.0019
r – correlation coefficient		1.00	0.99	0.99	0.97
<b>Herschel-Bulkley:</b>					
$\tau_H$ - the yield stress (Pa)		n/a	n/a	n/a	0.01
k - the Herschel-Bulkely consistency coefficient (Pa·s <sup>-b</sup> )		n/a	n/a	n/a	0.0049
b - the Hershel-Bulkely power-law exponent		n/a	n/a	n/a	0.84
r – correlation coefficient		n/a	n/a	n/a	0.98
n/a = not applicable					

## Physical Property Data

Physical Property	B-203	B-203	B-203	B-203	B-203
Source of Data	<i>PNNL-14365</i>	<i>PNNL-14365</i>	<i>PNNL-14365</i>	<i>PNNL-14365</i>	<i>PNNL-14365</i>
Temperature (°C)					
Zeta Potential (mV)					
Bulk Density (g/mL)	1.28	1.26	1.18	1.18	1.06
vol% Settled Solids	100	100	87.5	87.5	43.8
Density of Centrifuged Solids (g/mL)	1.53	1.41	1.38	1.38	1.52
vol% Centrifuged Solids	83.7	54.5	38.5	38.5	13.9
wt% Centrifuged Solids	<i>100</i>	<i>61</i>	<i>45</i>	<i>45</i>	<i>20</i>
Supernatant Density (g/mL)	1.21	1.15	1.10	1.10	1.04
Density of Settled Solids (g/mL)					
wt% Settled Supernatant					
wt% dissolved solids in supernatant					
wt% total solids in Centrifuged Sludge					
wt% Total Solids	40.5	28.6	19.7	19.7	8.5
wt% UDS	<i>7.00</i>	<i>11.03</i>	<i>8.47</i>	<i>8.47</i>	<i>2.32</i>
Density of Solids (g/cc)	5.52	5.52	5.52	5.52	5.52

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Settling Data**

Settling Schedule		PNNL-14365	PNNL-14365	PNNL-14365	PNNL-14365
Source of Data					
Temperature (°C)					
Total initial volume			13.3	13.3	13
5 minutes			13.3	13.3	12.6
10 minutes			13.3	13.3	12.1
15 minutes			13.3	13.3	11.4
20 minutes			13.3	13.3	10.6
30 minutes			13.3	13.3	9.5
40 minutes					
50 minutes					
1 hour			13.3	13.3	7.3
2 hours			13.05	13.05	6.2
3 hours			13	13	6
4 hours			12.95	12.95	5.9
5 hours					
6 hours			12.7	12.7	5.7
24 hours			12	12	5.6
32 hours					5.6
48 hours			11.8	11.8	5.6
56 hours			11.7	11.7	5.6
72 hours final settled			11.7	11.7	5.6

**Shear Strength Data**

Shear Strength Schedule	B-203	B-203			
Source of Data	PNNL-14365	PNNL-14365			
Instrumentation	Haake RS300 Shear Vane	Haake RS300 Shear Vane			
Temperature (°C)	25	25			
Description	Homogenized Tank Composite	30 wt% dilution of the tank composite			
Gelation Time/Shear Strength (Pa)					
5 minutes					
10 minutes					
15 minutes					
20 minutes					
30 minutes					
40 minutes					
50 minutes					
1 hour					
2 hours					
3 hours					
4 hours					
5 hours					
6 hours					
24 hours					
32 hours					
48 hours					
56 hours					
72 hours	2280	60			
Infinte time (GRE)					

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.





**Physical Property Data**

Physical Property	BX-107	BX-107	BX-107	BX-107	BX-107	BX-107	BX-107	BX-107	BX-107	BX-107	BX-107	BX-107	BX-107	BX-107	BX-107	BX-107	BX-107	BX-107	
Notes																			
Temperature (°C)	25	25	25	25	25	25	25	25	25	25	25	25	25	25	25	25	25	25	25
Zeta Potential (mV)																			
Bulk Density (g/mL)	1.47	1.47	<i>1.17</i>	<i>1.17</i>	<i>1.06</i>	<i>1.06</i>	1.45	1.45	<i>1.17</i>	<i>1.17</i>	<i>1.06</i>	<i>1.06</i>	1.4	1.4	<i>1.17</i>	<i>1.17</i>	<i>1.06</i>	<i>1.06</i>	
vol% Settled Solids	100	100	n/m	n/m	n/m	n/m	100	100	n/m	n/m	n/m	n/m	97.8	97.8	n/m	n/m	n/m	n/m	
Density of Centrifuged Solids (g/mL)	1.58	1.58	n/m	n/m	n/m	n/m	1.54	1.54	n/m	n/m	n/m	n/m	1.49	1.49	n/m	n/m	n/m	n/m	
vol% Centrifuged Solids	71.7	71.7	n/m	n/m	n/m	n/m	76	76	n/m	n/m	n/m	n/m	66	66	n/m	n/m	n/m	n/m	
wt% Centrifuged Solids	77.2	77.2	n/m	n/m	n/m	n/m	80.6	80.6	n/m	n/m	n/m	n/m	70.4	70.4	n/m	n/m	n/m	n/m	
Supernatant Density (g/mL)	1.18	1.18	<i>1.11</i>	<i>1.11</i>	<i>1.05</i>	<i>1.05</i>	1.17	1.17	<i>1.11</i>	<i>1.11</i>	<i>1.05</i>	<i>1.05</i>	1.21	1.21	<i>1.12</i>	<i>1.12</i>	<i>1.06</i>	<i>1.06</i>	
Density of Settled Solids (g/mL)	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	
wt% Settled Supernatant	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	
wt% dissolved solids in supernatant	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	
wt% total solids in Centrifuged Sludge	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	
wt% Total Solids	44.8	44.8	n/m	n/m	n/m	n/m	45.6	45.6	n/m	n/m	n/m	n/m	42	42	n/m	n/m	n/m	n/m	
wt% UDS	38.00	38.00	<i>7.54</i>	<i>7.54</i>	<i>1.50</i>	<i>1.50</i>	39.60	39.60	<i>7.85</i>	<i>7.85</i>	<i>1.56</i>	<i>1.56</i>	32.60	32.60	<i>6.47</i>	<i>6.47</i>	<i>1.28</i>	<i>1.28</i>	
Density of Solids (g/cc)	<i>2.07</i>	<i>2.07</i>	<i>3.44</i>	<i>3.44</i>	<i>3.44</i>	<i>3.44</i>	<i>2.07</i>	<i>2.07</i>	<i>3.44</i>	<i>3.44</i>	<i>3.44</i>	<i>3.44</i>	<i>2.07</i>	<i>2.07</i>	<i>3.44</i>	<i>3.44</i>	<i>3.44</i>	<i>3.44</i>	

**Settling Data**

Settling Schedule		BX-107		BX-107		BX-107		BX-107		BX-107		BX-107		BX-107		BX-107	
Notes:			C04-001-7		C04-001-7			C04-001-8		C04-001-8			C04-001-9		C04-001-9		C04-001-9
Temperature (°C)			25		25			25		25			25		25		25
Total initial volume			100		100			100		100			100		100		100
5 minutes																	
10 minutes																	
15 minutes																	
20 minutes																	
30 minutes																	
40 minutes																	
50 minutes																	
1 hour																	
2 hours			82		55			87		55			85		60		
3 hours																	
4 hours																	
5 hours			76		50			80		49			67		40		
6 hours																	
24 hours			67		42			70		39			57		32		
32 hours			65		40			67		38			55		31		
48 hours			64		39			66		35			53		31		
56 hours			63		38			66		35			52		31		
72 hours final settled																	

**Shear Strength Data**

Shear Strength Schedule	BX-107	BX-107	BX-107	BX-107	BX-107	BX-107	BX-107	BX-107	BX-107	BX-107	BX-107	BX-107	BX-107	BX-107	BX-107	BX-107	BX-107	BX-107
Source of Data	SST BX-107 Cores 40 and 41 data package	SST BX-107 Cores 40 and 41 data package	SST BX-107 Cores 40 and 41 data package	SST BX-107 Cores 40 and 41 data package	SST BX-107 Cores 40 and 41 data package	SST BX-107 Cores 40 and 41 data package	SST BX-107 Cores 40 and 41 data package	SST BX-107 Cores 40 and 41 data package	SST BX-107 Cores 40 and 41 data package	SST BX-107 Cores 40 and 41 data package	SST BX-107 Cores 40 and 41 data package	SST BX-107 Cores 40 and 41 data package	SST BX-107 Cores 40 and 41 data package	SST BX-107 Cores 40 and 41 data package	SST BX-107 Cores 40 and 41 data package	SST BX-107 Cores 40 and 41 data package	SST BX-107 Cores 40 and 41 data package	SST BX-107 Cores 40 and 41 data package
Notes:	Page C04-001-6																	
Temperature (°C)	Ambient																	
Description																		
Gelation Time/Shear Strength (Pa)																		
5 minutes	300						880						480					
10 minutes																		
15 minutes																		
20 minutes																		
30 minutes																		
40 minutes																		
50 minutes																		
1 hour																		
2 hours																		
3 hours																		
4 hours																		
5 hours																		
6 hours																		
24 hours																		
32 hours																		
48 hours																		
56 hours																		
72 hours																		
Infinite time (GRE)																		



Rheological Data

Model/model Parameter	C-104				C-104				C-104				C-104				C-104			
Temperature (°C)	25				25				25				25				25			
Source of Data	BNFL-RPT-030 Rev. 0	BNFL-RPT-030 Rev. 0	BNFL-RPT-030 Rev. 0	BNFL-RPT-030 Rev. 0	RPP-5798	RPP-5798	RPP-5798	RPP-5798	RPP-5798	RPP-5798	RPP-5798	RPP-5798	RPP-5798	RPP-5798	RPP-5798	RPP-5798	RPP-5798	RPP-5798		
Notes	Appendix F; Figure 5	Appendix F; Figure 7	Appendix F; Figure 13	Appendix F; Figure 16	Table 3-2	Table 3-2	Table 3-2	Table 3-2	Table 3-2	Table 3-2	Table 3-2	Table 3-2	Table 3-2	Table 3-2	Table 3-2	Page A-3	Page A-8	Page A-13	Page A-18	
<b>Newtonian:</b>																				
$\eta$ - Newtonian viscosity (cP)	1.704	103.647	15.54	8.51	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	30.160	15.541	12.819	2.538	
$r$ - correlation coefficient	0.992	0.939	0.94	1.00	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	0.965	0.980	0.972	0.917	
<b>Ostwald (or Power Law):</b>																				
$m$ - the consistency coefficient (Pa·s <sup>n</sup> )	0.002	16.879	0.02	0.04	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	1.709	1.165	1.174	0.021	
$n$ - the power-law exponent	1.000	0.046	1.00	0.77	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	0.256	0.199	0.162	0.609	
$r$ - correlation coefficient	0.992	0.696	0.94	1.00	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	0.981	0.948	0.935	0.979	
<b>Bingham Plastic:</b>																				
$\tau_0$ - the Bingham yield stress (Pa)	0.000	20.445	1.77	2.49	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	4.311	2.083	1.871	0.172	
$\eta_p$ - the plastic viscosity (Pa·s)	0.002	0.001	0.01	0.01	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	0.010	0.006	0.004	0.002	
$r$ - correlation coefficient	0.992	0.939	0.94	1.00	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	0.965	0.980	0.972	0.917	
<b>Herschel-Bulky:</b>																				
$\tau_0$ - the yield stress (Pa)	0.000	16.838	2.35	2.39	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	4.172	1.927	1.728	0.042	
$k$ - the Herschel-Bulky consistency coefficient (Pa·s <sup>n</sup> )	0.002	0.083	0.00	0.01	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	0.024	0.023	0.022	0.026	
$b$ - the Herschel-Bulky power-law exponent	1.000	0.799	1.00	0.99	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	0.857	0.772	0.718	0.560	
$r$ - correlation coefficient	0.992	0.911	0.94	1.00	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	0.981	0.992	0.984	0.985	
n/a = not applicable																				

Physical Property Data

Physical Property	C-104				C-104				C-104				C-104				C-104			
Notes																				
Temperature (°C)	25				25				25				25				25			
Zeta Potential (mV)																				
Bulk Density (g/mL)	1.06	1.22	1.16	1.14	1.55	1.55	1.55	1.55	1.55	1.55	1.55	1.55	1.55	1.55	1.55	1.55	1.55	1.55	1.104	
vol% Settled Solids	29.1	93.8	95	95.2	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	
Density of Centrifuged Solids (g/mL)	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	
vol% Centrifuged Solids	11	46.2	50.6	42.2	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	
wt% Centrifuged Solids	14.7	54.2	58.3	50.9	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	
Supernatant Density (g/mL)	1.02	1.001	1.001	1.001	<i>1.24</i>	<i>1.24</i>	<i>1.24</i>	<i>1.24</i>	<i>1.24</i>	<i>1.24</i>	<i>1.24</i>	<i>1.24</i>	<i>1.24</i>	<i>1.24</i>	<i>1.24</i>	<i>1.24</i>	<i>1.24</i>	<i>1.24</i>	1.04	
Density of Settled Solids (g/mL)	1.2	1.28	1.18	1.18	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	1.226	
wt% Settled Supernatant	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	
wt% dissolved solids in supernatant	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	
wt% total solids in Centrifuged Sludge	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	
wt% Total Solids	9.7	24.9	22.1	21.2	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	
wt% UDS	6.90	24.00	22.00	20.50	<i>34.26</i>	<i>34.26</i>	<i>34.26</i>	<i>34.26</i>	<i>34.26</i>	<i>34.26</i>	<i>34.26</i>	<i>34.26</i>	<i>34.26</i>	<i>34.26</i>	<i>34.26</i>	<i>34.26</i>	<i>34.26</i>	<i>34.26</i>	<i>8.66</i>	
Density of Solids (g/cc)	<i>3.03</i>	<i>3.15</i>	<i>3.15</i>	<i>4.18</i>	<i>3.03</i>	<i>3.03</i>	<i>3.03</i>	<i>3.03</i>	<i>3.03</i>	<i>3.03</i>	<i>3.03</i>	<i>3.03</i>	<i>3.03</i>	<i>3.03</i>	<i>3.03</i>	<i>3.03</i>	<i>3.03</i>	<i>3.03</i>	<i>3.15</i>	

**Settling Data**

Settling Schedule	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104
Notes:																		
Temperature (°C)	25	25	25	25	25	25	25	25	25	25	25	25	25	25	25	25	25	25
Total initial volume																		99
5 minutes																		
10 minutes																		
15 minutes																		
20 minutes																		98
30 minutes																		
40 minutes																		97
50 minutes																		
1 hour																		95
2 hours																		88
3 hours																		82
4 hours																		76
5 hours																		71
6 hours																		66
24 hours																		49
32 hours																		43
48 hours																		38
56 hours																		37
72 hours final settled																		34

**Shear Strength Data**

Shear Strength Schedule					C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104				
Source of Data					RPP-5798, Rev.0B	RPP-5798, Rev.0B	RPP-5798, Rev.0B	RPP-5798, Rev.0B	RPP-5798, Rev.0B	RPP-5798, Rev.0B	RPP-5798, Rev.0B	RPP-5798, Rev.0B	RPP-5798, Rev.0B	RPP-5798, Rev.0B				
Notes:					HNF-1666 Rev.0B	HNF-1666 Rev.0B	HNF-1666 Rev.0B	HNF-1666 Rev.0B	HNF-1666 Rev.0B	HNF-1666 Rev.0B	HNF-1666 Rev.0B	HNF-1666 Rev.0B	HNF-1666 Rev.0B	HNF-1666 Rev.0B				
Temperature (°C)																		
Description					Shear Vane, on core 247 segment 1 upper solids; 6 months undisturbed	Shear Vane, on core 247 segment 1 lower solids; 6 months undisturbed	Shear Vane, on core 247 segment 2 upper solids; 6 months undisturbed	Shear Vane, on core 247 segment 2 lower solids; 6 months undisturbed	Shear Vane, on core 247 segment 3 quarter A; 6 months undisturbed	Shear Vane, on core 247 segment 3 quarter B; 6 months undisturbed	Shear Vane, on core 247 segment 3 quarter C; 6 months undisturbed	Shear Vane, on core 247 segment 3 quarter D; 6 months undisturbed	Shear Vane, on core 247 segment 4 upper solids; 6 months undisturbed	Shear Vane, on core 247 segment 4 lower solids; 6 months undisturbed				
Gelation Time/Shear Strength (Pa)																		
5 minutes																		
10 minutes																		
15 minutes																		
20 minutes																		
30 minutes																		
40 minutes																		
50 minutes																		
1 hour																		
2 hours																		
3 hours																		
4 hours																		
5 hours																		
6 hours																		
24 hours																		
32 hours																		
48 hours																		
56 hours																		
72 hours																		
Infinite time (GRE)					345	289	521	2421	885	1304	791	2607	810	7077				

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.



Rheological Data

Model/model Parameter	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	
Temperature (°C)	45	65	25	45	65	25	45	65	25	45	65	25	45	65	25	45	
Source of Data	RPP-5798	RPP-5798	RPP-5798	RPP-5798	RPP-5798	RPP-5798	RPP-5798	RPP-5798	RPP-5798	RPP-5798	RPP-5798	RPP-5798	RPP-5798	RPP-5798	RPP-5798	RPP-5798	
Notes	Page A-23	Page A-28	Page A-33	Page A-38	Page A-28	Page A-48	Page A-53	Page A-28	Page A-63	Page A-68	Page A-73	Page A-78	Page A-83	Page A-88	Page A-93	Page A-83	Page A-88
<b>Newtonian:</b>																	
η - Newtonian viscosity (cP)	1.987	1.561	1.339	1.339	1.373	2.115	1.269	1.134	4.892	3.808	2.898	6.758	6.571	6.013	23.632	24.832	25.055
r - correlation coefficient	0.996	0.991	0.983	0.983	0.982	0.990	0.961	0.971	0.944	0.984	0.993	0.917	0.924	0.960	0.977	0.955	0.989
<b>Ostwald (or Power Law):</b>																	
m - the consistency coefficient (Pas <sup>n</sup> )	0.006	0.008	0.003	0.003	0.001	0.024	0.001	0.001	0.106	0.086	0.122	0.274	0.387	0.372	1.292	1.853	2.509
n - the power-law exponent	0.812	0.711	0.852	0.852	1.000	0.554	0.996	1.000	0.433	0.425	0.307	0.317	0.246	0.235	0.260	0.201	0.144
r - correlation coefficient	0.998	0.965	0.972	0.972	0.982	0.953	0.960	0.971	0.994	0.974	0.938	0.993	0.996	0.905	0.971	0.982	0.903
<b>Bingham Plastic:</b>																	
τ <sub>0</sub> - the Bingham yield stress (Pa)	0.093	0.082	0.027	0.027	0.007	0.150	0.024	0.000	0.381	0.304	0.302	0.707	0.804	0.736	2.776	3.348	3.786
η <sub>p</sub> - the plastic viscosity (Pas)	0.002	0.001	0.001	0.001	0.001	0.001	0.001	0.001	0.003	0.002	0.001	0.003	0.003	0.003	0.011	0.009	0.008
r - correlation coefficient	0.996	0.991	0.983	0.983	0.982	0.990	0.961	0.971	0.944	0.984	0.993	0.917	0.924	0.960	0.977	0.955	0.989
<b>Herschel-Bulkley:</b>																	
τ <sub>0</sub> - the yield stress (Pa)	0.066	0.078	0.026	0.026	0.007	0.067	0.017	0.000	0.381	0.286	0.279	0.653	0.588	0.653	2.497	2.904	3.591
k - the Herschel-Bulkely consistency coefficient (Pas <sup>n</sup> )	0.005	0.001	0.001	0.001	0.001	0.016	0.001	0.001	0.004	0.004	0.004	0.008	0.045	0.013	0.041	0.075	0.029
n - the Herschel-Bulkely power-law exponent	0.811	1.000	1.000	1.000	1.000	0.602	1.000	1.000	0.970	0.920	0.845	0.855	0.548	0.731	0.774	0.655	0.771
r - correlation coefficient	0.998	0.991	0.983	0.983	0.982	0.960	0.961	0.971	0.948	0.989	0.995	0.943	0.988	0.967	0.993	0.992	0.994
n/a = not applicable																	

Physical Property Data

Physical Property	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	C-104	
Notes																	
Temperature (°C)	45	65	25	45	65	25	45	65	25	45	65	25	45	65	25	45	
Zeta Potential (mV)																	
Bulk Density (g/mL)	1.104	1.104	<i>1.24</i>	<i>1.24</i>	<i>1.24</i>	1.068	1.068	1.068	1.159	1.159	1.159	1.24	1.24	1.24	1.36	1.36	1.36
vol% Settled Solids	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
Density of Centrifuged Solids (g/mL)	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
vol% Centrifuged Solids	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% Centrifuged Solids	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
Supernatant Density (g/mL)	1.04	1.04	<i>1.24</i>	<i>1.24</i>	<i>1.24</i>	1.02	1.02	1.02	1.05	1.05	1.05	<i>1.11</i>	<i>1.11</i>	<i>1.11</i>	<i>1.17</i>	<i>1.17</i>	<i>1.17</i>
Density of Settled Solids (g/mL)	1.226	1.226	n/m	1.243	1.243	1.243	1.243	1.243	1.308	1.308	1.308	1.243	1.243	1.243	n/m	n/m	n/m
wt% Settled Supernatant	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% dissolved solids in supernatant	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% total solids in Centrifuged Sludge	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% Total Solids	<i>8.66</i>	<i>8.66</i>	<i>0.00</i>	<i>0.00</i>	<i>0.00</i>	<i>6.24</i>	<i>6.24</i>	<i>6.24</i>	<i>13.87</i>	<i>13.87</i>	<i>13.87</i>	<i>16.13</i>	<i>16.13</i>	<i>16.13</i>	<i>22.06</i>	<i>22.06</i>	<i>22.06</i>
wt% UDS	<i>3.15</i>	<i>3.15</i>	<i>3.03</i>	<i>3.03</i>	<i>3.03</i>	<i>3.15</i>	<i>3.15</i>	<i>3.15</i>	<i>3.15</i>	<i>3.15</i>	<i>3.15</i>	<i>3.15</i>	<i>3.15</i>	<i>3.15</i>	<i>3.15</i>	<i>3.15</i>	<i>3.15</i>
Density of Solids (g/cc)	<i>3.15</i>	<i>3.15</i>	<i>3.03</i>	<i>3.03</i>	<i>3.03</i>	<i>3.15</i>	<i>3.15</i>	<i>3.15</i>	<i>3.15</i>	<i>3.15</i>	<i>3.15</i>	<i>3.15</i>	<i>3.15</i>	<i>3.15</i>	<i>3.15</i>	<i>3.15</i>	<i>3.15</i>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

Settling Data

Settling Schedule	<i>C-104</i>	<i>C-104</i>	<i>C-104</i>	<i>C-104</i>	<i>C-104</i>	<i>C-104</i>	<i>C-104</i>	<i>C-104</i>	<i>C-104</i>	<i>C-104</i>	<i>C-104</i>	<i>C-104</i>	<i>C-104</i>	<i>C-104</i>	<i>C-104</i>	<i>C-104</i>
Notes:																
Temperature (°C)	25	25	25	25	25	25	25	25	25	25	25	25	25	25	25	25
Total initial volume						100			100							
5 minutes																
10 minutes																
15 minutes																
30 minutes						94			98							
30 minutes																
40 minutes						86			98							
50 minutes																
1 hour						83			97							
2 hours						85			95							
3 hours						79			90							
4 hours						49			83							
5 hours						41			79							
6 hours						38			76							
24 hours						25			60							
32 hours						23			55							
48 hours						22			50							
56 hours						22			48							
72 hours final settled						21			42							

Shear Strength Data

Shear Strength Schedule																
Source of Data																
Notes:																
Temperature (°C)																
Description																
Gelation Time/Shear Strength (Pa)																
5 minutes																
10 minutes																
15 minutes																
20 minutes																
30 minutes																
40 minutes																
50 minutes																
1 hour																
2 hours																
3 hours																
4 hours																
5 hours																
6 hours																
24 hours																
32 hours																
48 hours																
56 hours																
72 hours																
Infinite time (GRE)																

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.



## Model Chemical Data From ESP

Analyte/Sample	C-109	C-109	C-109
Description	no dilution	1:1 dilution	3:1 dilution
Model Basis	Salty	Salt Free	Salt Free
Report No./Source of Data	WHC-SD-WM-ER-402, rev 0; Core 47	WHC-SD-WM-ER-402, rev 0; Core 47	WHC-SD-WM-ER-402, rev 0; Core 47
Solid Phases (vol% of bulk)			
(NaAlO <sub>2</sub> ) <sub>2</sub> ·2.5H <sub>2</sub> O	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	-	-	-
Bi <sub>2</sub> O <sub>3</sub>	<i>0.01311</i>	<i>0.01166</i>	<i>0.00711</i>
BiOCl	-	-	-
Boehmite	-	-	-
Ca(OH) <sub>2</sub>	-	-	-
Ca <sub>3</sub> OH(PO <sub>4</sub> ) <sub>3</sub>	<i>0.41412</i>	<i>0.36843</i>	<i>0.22460</i>
CaC <sub>2</sub> O <sub>4</sub> ·H <sub>2</sub> O	-	-	-
CaCO <sub>3</sub>	-	-	-
CaF <sub>2</sub>	-	-	-
CrOOH	<i>0.00285</i>	<i>0.00254</i>	<i>0.00155</i>
FeOOH	<i>0.22392</i>	<i>0.19921</i>	<i>0.12144</i>
Gibbsite	<i>1.96610</i>	<i>1.74915</i>	<i>1.06632</i>
HgO	-	-	-
KAlSiO <sub>4</sub>	-	-	-
La(OH) <sub>3</sub>	-	-	-
LaPO <sub>4</sub> ·2H <sub>2</sub> O	<i>0.00007</i>	<i>0.00006</i>	<i>0.00004</i>
Mn(OH) <sub>2</sub>	-	-	-
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	<i>0.00459</i>	<i>0.00409</i>	<i>0.00249</i>
MnCO <sub>3</sub>	-	-	-
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	<i>0.08836</i>	<i>0.07861</i>	<i>0.04792</i>
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	<i>0.70261</i>	<i>0.62508</i>	<i>0.38106</i>
NaAlSiO <sub>4</sub>	<i>0.37371</i>	<i>0.33247</i>	<i>0.20268</i>
Ni(OH) <sub>2</sub>	<i>0.16172</i>	<i>0.14388</i>	<i>0.08771</i>
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-
NiC <sub>2</sub> O <sub>4</sub> ·2H <sub>2</sub> O	-	-	-
Pb(OH) <sub>2</sub>	<i>0.01165</i>	<i>0.01036</i>	<i>0.00632</i>
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-
PbCO <sub>3</sub>	-	-	-
Pu(OH) <sub>4</sub>	<i>0.00002</i>	<i>0.00002</i>	<i>0.00001</i>
SiO <sub>2</sub>	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-
SrCO <sub>3</sub>	<i>0.00548</i>	<i>0.00487</i>	<i>0.00297</i>
TcO <sub>2</sub>	-	-	-
ZrO <sub>2</sub>	<i>0.00022</i>	<i>0.00020</i>	<i>0.00012</i>
KNO <sub>3</sub>	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	<i>0.07715</i>	-	-
Na <sub>2</sub> CO <sub>3</sub> ·H <sub>2</sub> O	-	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-	-
Na <sub>2</sub> SO <sub>4</sub> ·10H <sub>2</sub> O	-	-	-
Na <sub>3</sub> FSO <sub>4</sub>	-	-	-
Na <sub>3</sub> NO <sub>3</sub> SO <sub>4</sub> ·H <sub>2</sub> O	-	-	-
Na <sub>3</sub> PO <sub>4</sub> ·8H <sub>2</sub> O	-	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> ·10H <sub>2</sub> O	-	-	-
Na <sub>6</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-	-
NaF	-	-	-
NaF(PO <sub>4</sub> ) <sub>2</sub> ·19H <sub>2</sub> O	<i>1.26441</i>	-	-
NaHCO <sub>3</sub>	-	-	-
NaNO <sub>2</sub>	-	-	-
NaNO <sub>3</sub>	-	-	-
Na <sub>3</sub> PO <sub>4</sub> ·0.25NaOH·12H <sub>2</sub> O	<i>1.31565</i>	-	-
Total Volume % UDS	<i>6.63</i>	<i>3.53</i>	<i>2.15</i>
Solids Concentration (g/L)	<b><i>156.2</i></b>	<b><i>98.7</i></b>	<b><i>60.2</i></b>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

### Rheological Data

Model/model Parameter		<i>C-109</i>	<i>C-109</i>
Temperature (°C)		30	30
Source of Data		WHC-SD-WM-ER-402, rev 0; Core 47	WHC-SD-WM-ER-402, rev 0; Core 47
Notes		Entered from Joel Tingey's Paper File	Entered from Joel Tingey's Paper File
<b>Newtonian:</b>			
$\eta$ – Newtonian viscosity (cP)		164.527	5.490
r – correlation coefficient		0.558	0.896
<b>Ostwald (or Power Law):</b>			
m – the consistency coefficient (Pa·s <sup>-n</sup> )		20.278	0.512
n – the power-law exponent		0.186	0.215
r – correlation coefficient		0.805	0.911
<b>Bingham Plastic:</b>			
$\tau_B$ - the Bingham yield stress (Pa)		37.203	0.929
$\eta_p$ - the plastic viscosity (Pa·s)		0.057	0.003
r – correlation coefficient		0.558	0.896
<b>Herschel-Bulkley:</b>			
$\tau_H$ - the yield stress (Pa)		16.131	0.906
k - the Herschel-Bulkely consistency coefficient (Pa·s <sup>-b</sup> )		7.214	0.004
b - the Hershel-Bulkely power-law exponent		0.311	0.943
r – correlation coefficient		0.761	0.902
n/a = not applicable			

### Physical Property Data

Physical Property	<i>C-109</i>	<i>C-109</i>	<i>C-109</i>
Notes			
Temperature (°C)	30	30	30
Zeta Potential (mV)			
Bulk Density (g/mL)	1.23	<i>1.19</i>	1.11
vol% Settled Solids	100	88	41
Density of Centrifuged Solids (g/mL)	<i>1.23</i>	n/m	1.39
	100	n/m	21.1
vol% Centrifuged Solids	100	n/m	27
wt% Centrifuged Solids			
Supernatant Density (g/mL)	1.15	<i>1.13</i>	1.01
Density of Settled Solids (g/mL)	n/m	n/m	n/m
wt% Settled Supernatant	n/m	n/m	n/m
wt% dissolved solids in supernatant	<i>29.61</i>	<i>29.12</i>	<i>26.01</i>
wt% total solids in Centrifuged Sludge	n/m	n/m	n/m
wt% Total Solids	n/m	n/m	n/m
wt% UDS	<i>12.70</i>	<i>8.30</i>	<i>5.42</i>
Density of Solids (g/cc)	<i>2.36</i>	<i>2.80</i>	<i>2.80</i>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Settling Data**

Settling Schedule		<i>C-109</i>	<i>C-109</i>
Notes:		Page B-19; appears to be fast settling	Page B-19; appears to be fast settling
Temperature (°C)		30	30
Total initial volume		100	100
5 minutes			
10 minutes			
15 minutes			
20 minutes			
30 minutes			
40 minutes			
50 minutes			
1 hour			
2 hours		97	63
3 hours			
4 hours			
5 hours		92	59
6 hours			
24 hours		88	45
32 hours			
48 hours		87	40
56 hours		86	39
72 hours final settled			

**Shear Strength Data**

Shear Strength Schedule	<i>C-109</i>		
Source of Data	SG McKinley et al Characterization Report March 30, 1993		
Notes:			
Temperature (°C)	Unspecified		
Description	Shear Vane at unspecified gel time or temperature		
Gelation Time/Shear Strength (Pa)			
5 minutes			
10 minutes			
15 minutes			
20 minutes			
30 minutes			
40 minutes			
50 minutes			
1 hour			
2 hours			
3 hours			
4 hours			
5 hours			
6 hours			
24 hours			
32 hours			
48 hours			
56 hours			
72 hours	1730		
Infinte time (GRE)			

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

Model Chemical Data From ESP

Analyte/Sample	C-110	C-110	C-110	C-110	C-110	C-110	C-110	C-110	C-110	C-110	C-110
Description	Segment 2 no dilution	Segment 2 1:1 dilution	Segment 2 3:1 dilution	Segment 2 1:1 dilution	Segment 2 3:1 dilution	Segment 4 no dilution	Segment 4 1:1 dilution	Segment 4 3:1 dilution	Segment 4 1:1 dilution	Segment 4 3:1 dilution	Segment 4 3:1 dilution
Model Basis	Salty	Salt Free	Salt Free	Salt Free	Salt Free	Salty	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free
Report No/Source of Data	C-110 Cores 37, 38 and 39 data package.pdf	C-110 Cores 37, 38 and 39 data package.pdf	C-110 Cores 37, 38 and 39 data package.pdf	C-110 Cores 37, 38 and 39 data package.pdf	C-110 Cores 37, 38 and 39 data package.pdf	C-110 Cores 37, 38 and 39 data package.pdf	C-110 Cores 37, 38 and 39 data package.pdf	C-110 Cores 37, 38 and 39 data package.pdf	C-110 Cores 37, 38 and 39 data package.pdf	C-110 Cores 37, 38 and 39 data package.pdf	C-110 Cores 37, 38 and 39 data package.pdf
Solid Phases (vol% of bulk)											
(NaAlO <sub>2</sub> ) <sub>2</sub> •2.5H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	0.00002	0.00001	0.00000	0.00001	0.00000	0.00001	0.00001	0.00000	0.00001	0.00001	0.00000
Bi <sub>2</sub> O <sub>3</sub>	0.31812	0.16452	0.03037	0.16452	0.03037	0.19202	0.09388	0.01751	0.09388	0.01751	0.01751
BiOCl	-	-	-	-	-	-	-	-	-	-	-
Boehmite	-	-	-	-	-	-	-	-	-	-	-
Ca(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-
Ca <sub>5</sub> OH(PO <sub>4</sub> ) <sub>3</sub>	0.01181	0.00611	0.00113	0.00611	0.00113	0.00713	0.00349	0.00065	0.00349	0.00065	0.00065
CaC <sub>2</sub> O <sub>4</sub> •H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-
CaCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-
CaF <sub>2</sub>	0.10128	0.05238	0.00967	0.05238	0.00967	0.06114	0.02989	0.00558	0.02989	0.00558	0.00558
CrOOH	0.01912	0.00989	0.00183	0.00989	0.00183	0.01154	0.00564	0.00105	0.00564	0.00105	0.00105
FeOOH	0.63062	0.32614	0.06021	0.32614	0.06021	0.38066	0.18610	0.03472	0.18610	0.03472	0.03472
Gibbsite	1.24280	0.64273	0.11865	0.64273	0.11865	0.75018	0.36676	0.06842	0.36676	0.06842	0.06842
HgO	-	-	-	-	-	-	-	-	-	-	-
KAlSiO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-
La(OH) <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-
LaPO <sub>4</sub> •2H <sub>2</sub> O	0.00007	0.00003	0.00001	0.00003	0.00001	0.00004	0.00002	0.00000	0.00002	0.00000	0.00000
Mn(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	0.00565	0.00292	0.00054	0.00292	0.00054	0.00341	0.00167	0.00031	0.00167	0.00031	0.00031
MnCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	0.07967	0.04120	0.00761	0.04120	0.00761	0.04809	0.02351	0.00439	0.02351	0.00439	0.00439
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	0.45968	0.23773	0.04389	0.23773	0.04389	0.27747	0.13566	0.02531	0.13566	0.02531	0.02531
NaAlSiO <sub>4</sub>	2.02887	1.04926	0.19370	1.04926	0.19370	1.22467	0.59875	0.11169	0.59875	0.11169	0.11169
Ni(OH) <sub>2</sub>	0.00143	0.00074	0.00014	0.00074	0.00014	0.00087	0.00042	0.00008	0.00042	0.00008	0.00008
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-
NiC <sub>2</sub> O <sub>4</sub> •2H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-
Pb(OH) <sub>2</sub>	0.00579	0.00299	0.00055	0.00299	0.00055	0.00350	0.00171	0.00032	0.00171	0.00032	0.00032
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-
PbCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-
Pu(OH) <sub>4</sub>	0.00004	0.00002	0.00000	0.00002	0.00000	0.00002	0.00001	0.00000	0.00001	0.00000	0.00000
SiO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-
SrCO <sub>3</sub>	0.00924	0.00478	0.00088	0.00478	0.00088	0.00558	0.00273	0.00051	0.00273	0.00051	0.00051
TcO <sub>2</sub>	0.00003	0.00001	0.00000	0.00001	0.00000	0.00002	0.00001	0.00000	0.00001	0.00000	0.00000
ZrO <sub>2</sub>	0.00612	0.00316	0.00058	0.00316	0.00058	0.00369	0.00181	0.00034	0.00181	0.00034	0.00034
KNO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	0.01378	-	-	-	-	0.00832	-	-	-	-	-
Na <sub>2</sub> CO <sub>3</sub> •H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub> •10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> FSO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> NO <sub>3</sub> SO <sub>4</sub> •H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> •8H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> •10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-
Na <sub>4</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-
NaF	-	-	-	-	-	-	-	-	-	-	-
NaF(PO <sub>4</sub> ) <sub>2</sub> •19H <sub>2</sub> O	19.31784	-	-	-	-	11.66065	-	-	-	-	-
NaHCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> •0.25NaOH•12H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-
Total Volume % UDS	24.25	2.54	0.47	2.54	0.47	14.64	1.45	0.27	1.45	0.27	0.27
Solids Concentration (g/L)	497.7	82.4	15.2	82.4	15.2	300.4	47.0	8.8	47.0	8.8	8.8

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Rheological Data**

Model/model Parameter	C-110	C-110	C-110	C-110	C-110	C-110	C-110	C-110	C-110	C-110
Temperature (°C)	30	30	30	95	95	30	30	30	95	95
Source of Data	C-110 Cores 37, 38 and 39 data package.pdf	C-110 Cores 37, 38 and 39 data package.pdf	C-110 Cores 37, 38 and 39 data package.pdf	C-110 Cores 37, 38 and 39 data package.pdf	C-110 Cores 37, 38 and 39 data package.pdf	C-110 Cores 37, 38 and 39 data package.pdf	C-110 Cores 37, 38 and 39 data package.pdf	C-110 Cores 37, 38 and 39 data package.pdf	C-110 Cores 37, 38 and 39 data package.pdf	C-110 Cores 37, 38 and 39 data package.pdf
Notes		C04-077	C04-114	C04-085	C04-118		C04-093	C04-126	C04-104	C04-138
<b>Newtonian:</b>										
$\eta$ – Newtonian viscosity (cP)		4.937	2.160	2.251	1.376		3.637	2.144	3.156	1.824
r – correlation coefficient		0.998	1.000	0.985	0.978		0.997	1.000	0.998	0.983
<b>Ostwald (or Power Law):</b>										
m – the consistency coefficient (Pa·s <sup>-n</sup> )		0.011	0.003	0.011	0.001		0.013	0.002	0.049	0.012
n – the power-law exponent		0.858	0.924	0.733	1.000		0.777	0.998	0.533	0.681
r – correlation coefficient		0.997	0.998	0.945	0.978		0.991	1.000	0.940	0.927
<b>Bingham Plastic:</b>										
$\tau_B$ – the Bingham yield stress (Pa)		0.676	0.000	0.159	0.000		0.218	0.000	0.414	0.173
$\eta_p$ – the plastic viscosity (Pa·s)		0.003	0.002	0.002	0.001		0.003	0.002	0.002	0.001
r – correlation coefficient		0.998	1.000	0.985	0.978		0.997	1.000	0.998	0.983
<b>Herschel-Bulkley:</b>										
$\tau_H$ – the yield stress (Pa)		0.420	0.000	0.144	0.000		0.200	0.000	0.403	0.174
k – the Herschel-Bulkely consistency coefficient (Pa·s <sup>-n</sup> )		0.004	0.003	0.004	0.001		0.004	0.002	0.003	0.001
b – the Hershel-Bulkely power-law exponent		0.979	0.971	0.876	1.000		0.935	1.000	0.942	1.000
r – correlation coefficient		0.999	0.999	0.972	0.978		0.998	1.000	0.999	0.983
n/a = not applicable										

**Physical Property Data**

Physical Property	C-110	C-110	C-110	C-110	C-110	C-110	C-110	C-110	C-110	C-110
Notes										
Temperature (°C)	30	30	30	30	30	30	30	30	30	30
Zeta Potential (mV)										
Bulk Density (g/mL)	1.41	<i>1.16</i>	<i>1.06</i>	<i>1.16</i>	<i>1.06</i>	1.48	<i>1.15</i>	<i>1.06</i>	<i>1.15</i>	<i>1.06</i>
vol% Settled Solids	100	n/m	n/m	n/m	n/m	100	n/m	n/m	n/m	n/m
Density of Centrifuged Solids (g/mL)	1.49	n/m	n/m	n/m	n/m	1.59	n/m	n/m	n/m	n/m
vol% Centrifuged Solids	75.7	n/m	n/m	n/m	n/m	76.2	n/m	n/m	n/m	n/m
wt% Centrifuged Solids	80	n/m	n/m	n/m	n/m	81.6	n/m	n/m	n/m	n/m
Supernatant Density (g/mL)	1.15	<i>1.10</i>	<i>1.05</i>	<i>1.10</i>	<i>1.05</i>	1.13	<i>1.12</i>	<i>1.05</i>	<i>1.12</i>	<i>1.05</i>
Density of Settled Solids (g/mL)	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% Settled Supernatant	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% dissolved solids in supernatant	<i>26.69</i>	<i>25.57</i>	<i>24.29</i>	<i>25.57</i>	<i>24.29</i>	<i>26.23</i>	<i>25.91</i>	<i>24.46</i>	<i>25.91</i>	<i>24.46</i>
wt% total solids in Centrifuged Sludge	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% Total Solids	40.3	n/m	n/m	n/m	n/m	28.4	n/m	n/m	n/m	n/m
wt% UDS	35.30	<i>7.13</i>	<i>1.44</i>	<i>7.13</i>	<i>1.44</i>	20.30	<i>4.10</i>	<i>0.83</i>	<i>4.10</i>	<i>0.83</i>
Density of Solids (g/cc)	<i>2.05</i>	<i>3.24</i>	<i>3.24</i>	<i>3.24</i>	<i>3.24</i>	<i>2.05</i>	<i>3.24</i>	<i>3.24</i>	<i>3.24</i>	<i>3.24</i>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Settling Data**

Settling Schedule		<i>C-110</i>	<i>C-110</i>				<i>C-110</i>	<i>C-110</i>		
Notes:		<b>C04-31</b>	<b>C04-036</b>				<b>C04-59</b>	<b>C04-064</b>		
Temperature (°C)		30	30				30	30		
Total initial volume		100	100				100	100		
5 minutes										
10 minutes										
15 minutes										
20 minutes										
30 minutes										
40 minutes										
50 minutes										
1 hour										
2 hours		89	74				90	70		
3 hours										
4 hours										
5 hours		76	48				82	50		
6 hours										
24 hours		65	36				78	35		
32 hours		61	33				65	34		
48 hours		60	33				63	33		
56 hours		60	32				63	32		
72 hours final settled										

**Shear Strength Data**

Shear Strength Schedule	<i>C-110</i>	<i>C-110</i>	<i>C-110</i>	<i>C-110</i>	<i>C-110</i>	<i>C-110</i>	<i>C-110</i>	<i>C-110</i>	<i>C-110</i>	<i>C-110</i>
Source of Data	<i>C-110 Cores 37, 38 and 39 data package.pdf</i>	<i>C-110 Cores 37, 38 and 39 data package.pdf</i>	<i>C-110 Cores 37, 38 and 39 data package.pdf</i>	<i>C-110 Cores 37, 38 and 39 data package.pdf</i>	<i>C-110 Cores 37, 38 and 39 data package.pdf</i>	<i>C-110 Cores 37, 38 and 39 data package.pdf</i>	<i>C-110 Cores 37, 38 and 39 data package.pdf</i>	<i>C-110 Cores 37, 38 and 39 data package.pdf</i>	<i>C-110 Cores 37, 38 and 39 data package.pdf</i>	<i>C-110 Cores 37, 38 and 39 data package.pdf</i>
Notes:	Page C04-008					Page C04-008				
Temperature (°C)	Unspecified					Unspecified				
Description	Shear Vane at unspecified gel time or temperature					Shear Vane at unspecified gel time or temperature				
Gelation Time/Shear Strength (Pa)										
5 minutes										
10 minutes										
15 minutes										
20 minutes										
30 minutes										
40 minutes										
50 minutes										
1 hour										
2 hours										
3 hours										
4 hours										
5 hours										
6 hours										
24 hours										
32 hours										
48 hours										
56 hours										
72 hours	500					500				
Infinte time (GRE)										

## Model Chemical Data From ESP

Analyte/Sample	C-112	C-112	C-112	C-112
Description	Core 36 composite	Core Composite 1:1 dilution	Core Composite 3:1 dilution	Core Composite 3:1 dilution
Model Basis	Salty	Salt Free	Salt Free	Salt Free
Report No/Source of Data	SST C-112 Core 36 data package	SST C-112 Core 36 data package	SST C-112 Core 36 data package	SST C-112 Core 36 data package
Solid Phases (vol% of bulk)				
(NaAlO <sub>2</sub> ) <sub>2</sub> •2.5H <sub>2</sub> O	-	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	<i>0.00004</i>	<i>0.00001</i>	<i>0.00001</i>	<i>0.00001</i>
Bi <sub>2</sub> O <sub>3</sub>	<i>0.08264</i>	<i>0.03255</i>	<i>0.01208</i>	<i>0.01208</i>
BiOCl	-	-	-	-
Boehmite	-	-	-	-
Ca(OH) <sub>2</sub>	-	-	-	-
Ca <sub>5</sub> OH(PO <sub>4</sub> ) <sub>3</sub>	<i>3.02056</i>	<i>1.18982</i>	<i>0.44146</i>	<i>0.44146</i>
CaC <sub>2</sub> O <sub>4</sub> •H <sub>2</sub> O	-	-	-	-
CaCO <sub>3</sub>	-	-	-	-
CaF <sub>2</sub>	-	-	-	-
CrOOH	<i>0.00997</i>	<i>0.00393</i>	<i>0.00146</i>	<i>0.00146</i>
FeOOH	<i>1.65469</i>	<i>0.65179</i>	<i>0.24184</i>	<i>0.24184</i>
Gibbsite	<i>1.77648</i>	<i>0.69977</i>	<i>0.25964</i>	<i>0.25964</i>
HgO	-	-	-	-
KAlSiO <sub>4</sub>	-	-	-	-
La(OH) <sub>3</sub>	-	-	-	-
LaPO <sub>4</sub> •2H <sub>2</sub> O	<i>0.00435</i>	<i>0.00171</i>	<i>0.00064</i>	<i>0.00064</i>
Mn(OH) <sub>2</sub>	-	-	-	-
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	<i>0.02757</i>	<i>0.01086</i>	<i>0.00403</i>	<i>0.00403</i>
MnCO <sub>3</sub>	-	-	-	-
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	<i>1.84757</i>	<i>0.72777</i>	<i>0.27003</i>	<i>0.27003</i>
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	<i>4.59954</i>	<i>1.81179</i>	<i>0.67224</i>	<i>0.67224</i>
NaAlSiO <sub>4</sub>	<i>0.88887</i>	<i>0.35013</i>	<i>0.12991</i>	<i>0.12991</i>
Ni(OH) <sub>2</sub>	<i>0.96973</i>	<i>0.38198</i>	<i>0.14173</i>	<i>0.14173</i>
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-
NiC <sub>2</sub> O <sub>4</sub> •2H <sub>2</sub> O	-	-	-	-
Pb(OH) <sub>2</sub>	<i>0.07341</i>	<i>0.02892</i>	<i>0.01073</i>	<i>0.01073</i>
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-
PbCO <sub>3</sub>	-	-	-	-
Pu(OH) <sub>4</sub>	<i>0.00009</i>	<i>0.00004</i>	<i>0.00001</i>	<i>0.00001</i>
SiO <sub>2</sub>	-	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	<i>0.03066</i>	<i>0.01208</i>	<i>0.00448</i>	<i>0.00448</i>
SrCO <sub>3</sub>	-	-	-	-
TcO <sub>2</sub>	-	-	-	-
ZrO <sub>2</sub>	<i>0.00074</i>	<i>0.00029</i>	<i>0.00011</i>	<i>0.00011</i>
KNO <sub>3</sub>	-	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	<i>0.84145</i>	-	-	-
Na <sub>2</sub> CO <sub>3</sub> •H <sub>2</sub> O	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub> •10H <sub>2</sub> O	-	-	-	-
Na <sub>3</sub> FSO <sub>4</sub>	-	-	-	-
Na <sub>3</sub> NO <sub>3</sub> SO <sub>4</sub> •H <sub>2</sub> O	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> •8H <sub>2</sub> O	-	-	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> •10H <sub>2</sub> O	<i>7.23122</i>	-	-	-
Na <sub>6</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-	-	-
NaF	-	-	-	-
NaF(PO <sub>4</sub> ) <sub>2</sub> •19H <sub>2</sub> O	-	-	-	-
NaHCO <sub>3</sub>	-	-	-	-
NaNO <sub>2</sub>	-	-	-	-
NaNO <sub>3</sub>	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> •0.25NaOH•12H <sub>2</sub> O	-	-	-	-
Total Volume % UDS	<i>23.06</i>	<i>5.90</i>	<i>2.19</i>	<i>2.19</i>
Solids Concentration (g/L)	<b>653.9</b>	<b>197.7</b>	<b>73.4</b>	<b>73.4</b>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Rheological Data**

Model/model Parameter			<i>C-112</i>	<i>C-112</i>
Temperature (°C)			25	95
Source of Data			<i>SST C-112 Core 36 data package</i>	<i>SST C-112 Core 36 data package</i>
Notes			Page C04-029	Page C04-031
<b>Newtonian:</b>				
$\eta$ – Newtonian viscosity (cP)			5.880	2.872
r – correlation coefficient			0.954	0.978
<b>Ostwald (or Power Law):</b>				
m – the consistency coefficient (Pa·s <sup>-n</sup> )			0.158	0.061
n – the power-law exponent			0.440	0.480
r – correlation coefficient			0.979	0.949
<b>Bingham Plastic:</b>				
$\tau_B$ - the Bingham yield stress (Pa)			0.697	0.368
$\eta_p$ - the plastic viscosity (Pa·s)			0.004	0.002
r – correlation coefficient			0.954	0.978
<b>Herschel-Bulkley:</b>				
$\tau_H$ - the yield stress (Pa)			0.497	0.271
k - the Herschel-Bulkely consistency coefficient (Pa·s <sup>b</sup> )			0.044	0.016
b - the Herschel-Bulkely power-law exponent			0.612	0.650
r – correlation coefficient			0.997	0.982
n/a = not applicable				

**Physical Property Data**

Physical Property	<i>C-112</i>	<i>C-112</i>	<i>C-112</i>	<i>C-112</i>
Notes				
Temperature (°C)	32	32	32	32
Zeta Potential (mV)				
Bulk Density (g/mL)	1.70	1.24	1.11	1.11
vol% Settled Solids	100	74.4	42.4	42.4
Density of Centrifuged Solids (g/mL)	1.95	n/m	1.39	1.39
vol% Centrifuged Solids	83	n/m	21.4	21.4
wt% Centrifuged Solids	n/m	n/m	27	27
Supernatant Density (g/mL)	1.23	<i>1.09</i>	1.01	1.01
Density of Settled Solids (g/mL)		n/m	n/m	n/m
wt% Settled Supernatant	n/m	n/m	n/m	n/m
wt% dissolved solids in supernatant	<i>26.87</i>	<i>23.75</i>	<i>22.06</i>	<i>22.06</i>
wt% total solids in Centrifuged Sludge	n/m	n/m	n/m	n/m
wt% Total Solids	55	n/m	n/m	n/m
wt% UDS	<i>38.47</i>	<i>15.94</i>	<i>6.61</i>	<i>6.61</i>
Density of Solids (g/cc)	<i>2.84</i>	3.35	3.35	3.35

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.



**Settling Data**

Settling Schedule		<i>C-112</i>	<i>C-112</i>	
Notes:		<b>C04-001-7</b>	<b>C04-001-7</b>	
Temperature (°C)		<b>25</b>	<b>25</b>	
Total initial volume		100	100	
5 minutes				
10 minutes				
15 minutes				
20 minutes				
30 minutes				
40 minutes				
50 minutes				
1 hour				
2 hours		96	87	
3 hours				
4 hours				
5 hours		94	62	
6 hours				
24 hours		88	50	
32 hours		76	47	
48 hours		75	42	
56 hours		74	42	
72 hours final settled				

**Shear Strength Data**

Shear Strength Schedule	<i>C-112</i>			
Source of Data	<i>SST C-112 Core 36 data package</i>			
Notes:	<b>Page 1-14</b>			
Temperature (°C)	<b>Unspecified</b>			
Description	<b>Page 1-13, 1-14: 10 weeks undisturbed (1680 hrs), 1 hour in water bath at unspecified temperature</b>			
Gelation Time/Shear Strength (Pa)				
5 minutes				
10 minutes				
15 minutes				
20 minutes				
30 minutes				
40 minutes				
50 minutes				
1 hour				
2 hours				
3 hours				
4 hours				
5 hours				
6 hours				
24 hours				
32 hours				
48 hours				
56 hours				
72 hours	1600			
Infinte time (GRE)				

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.



Shear Strength Data

Shear Strength Schedule	S-102	S-102	S-102	S-102	S-102	S-102	S-102	S-102	S-102	S-102	S-102	S-102	S-102	S-102	S-102	S-102	S-102	S-102	S-102	S-102		
Source of Data	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249		
Instrumentation	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer		
Temperature (°C)	38	38	38	38	38	38	38	38	38	25	38	38	38	38	38	38	38	38	38	38		
Description	Riser 11 Composition higher in metal oxides and low solubility ions Depth from bottom of tank is 22 inches	Riser 11 Composition higher in metal oxides and low solubility ions Depth from bottom of tank is 35 inches	Riser 11 Composition higher in metal oxides and low solubility ions Depth from bottom of tank is 55 inches	Riser 11 Composition higher in metal oxides and low solubility ions Depth from bottom of tank is 73 inches	Riser 11 Depth from bottom of tank is 113 inches	Riser 11 Depth from bottom of tank is 130 inches	Riser 11 Depth from bottom of tank is 150 inches	Riser 11 Depth from bottom of tank is 168 inches	Riser 11 Depth from bottom of tank is 190 inches	Riser 11 Depth from bottom of tank is 190 inches	Riser 14 Composition higher in metal oxides and low solubility ions Depth from bottom of tank is 12 inches	Riser 14 Composition higher in metal oxides and low solubility ions Depth from bottom of tank is 38 inches	Riser 14 Composition higher in metal oxides and low solubility ions Depth from bottom of tank is 70 inches	Riser 14 Depth from bottom of tank is 80 inches	Riser 14 Depth from bottom of tank is 95 inches	Riser 14 Depth from bottom of tank is 108 inches	Riser 14 Depth from bottom of tank is 113 inches	Riser 14 Depth from bottom of tank is 120 inches	Riser 14 Depth from bottom of tank is 132 inches	Riser 14 Depth from bottom of tank is 152 inches	Riser 14 Depth from bottom of tank is 168 inches	Riser 14 Depth from bottom of tank is 190 inches
Gelation Time/Shear Strength (Pa)																						
5 minutes																						
10 minutes																						
15 minutes																						
20 minutes																						
30 minutes																						
40 minutes																						
50 minutes																						
1 hour																						
2 hours																						
3 hours																						
4 hours																						
5 hours																						
6 hours																						
24 hours																						
32 hours																						
48 hours																						
56 hours																						
72 hours																						
Infinite time (GRE)	800	1000	800	1000	800	500	190	170	500	600	800	800	450	70	300	50	50	500	130	130	100	

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

Model Chemical Data From ESP

Analyte/Sample	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104
Description	Segment 2 no dilution	Segment 2 1:1 dilution	Segment 2 1.3:1 dilution	Segment 2 3:1 dilution	Segment 2 1:1 dilution	Segment 2 1.3:1 dilution	Segment 2 3:1 dilution	Segment 4 no dilution	Segment 4 1:1 dilution	Segment 4 1.3:1 dilution	Segment 4 3:1 dilution	Segment 4 1:1 dilution	Segment 4 1.3:1 dilution	Segment 4 3:1 dilution
Model Basis	Salty	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free	Salty	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free
Report No./Source of Data	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031
Solid Phases (vol% of bulk)														
(NaAlO <sub>2</sub> ) <sub>2</sub> •2.5H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Bi <sub>2</sub> O <sub>3</sub>	<i>0.00004</i>	<i>0.00002</i>	<i>0.00002</i>	<i>0.00001</i>	<i>0.00002</i>	<i>0.00002</i>	<i>0.00001</i>	<i>0.00003</i>	<i>0.00001</i>	<i>0.00001</i>	<i>0.00000</i>	<i>0.00001</i>	<i>0.00001</i>	<i>0.00000</i>
BiOCl	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Boehmite	<i>18.05730</i>	<i>8.21608</i>	<i>7.00884</i>	<i>2.60431</i>	<i>8.21608</i>	<i>7.00884</i>	<i>2.60431</i>	<i>14.87210</i>	<i>6.70448</i>	<i>5.74189</i>	<i>2.14376</i>	<i>6.70448</i>	<i>5.74189</i>	<i>2.14376</i>
Ca(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca <sub>2</sub> OH(PO <sub>4</sub> ) <sub>3</sub>	<i>0.00747</i>	<i>0.00340</i>	<i>0.00290</i>	<i>0.00108</i>	<i>0.00340</i>	<i>0.00290</i>	<i>0.00108</i>	<i>0.00615</i>	<i>0.00277</i>	<i>0.00237</i>	<i>0.00089</i>	<i>0.00277</i>	<i>0.00237</i>	<i>0.00089</i>
CaC <sub>2</sub> O <sub>4</sub> •H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaCO <sub>3</sub>	<i>0.03180</i>	<i>0.01447</i>	<i>0.01234</i>	<i>0.00459</i>	<i>0.01447</i>	<i>0.01234</i>	<i>0.00459</i>	<i>0.02619</i>	<i>0.01181</i>	<i>0.01011</i>	<i>0.00378</i>	<i>0.01181</i>	<i>0.01011</i>	<i>0.00378</i>
CaF <sub>2</sub>	<i>0.00650</i>	<i>0.00296</i>	<i>0.00252</i>	<i>0.00094</i>	<i>0.00296</i>	<i>0.00252</i>	<i>0.00094</i>	<i>0.00535</i>	<i>0.00241</i>	<i>0.00207</i>	<i>0.00077</i>	<i>0.00241</i>	<i>0.00207</i>	<i>0.00077</i>
CrOOH	<i>0.03171</i>	<i>0.01443</i>	<i>0.01231</i>	<i>0.00457</i>	<i>0.01443</i>	<i>0.01231</i>	<i>0.00457</i>	<i>0.02611</i>	<i>0.01177</i>	<i>0.01008</i>	<i>0.00376</i>	<i>0.01177</i>	<i>0.01008</i>	<i>0.00376</i>
FeOOH	<i>0.09505</i>	<i>0.04325</i>	<i>0.03689</i>	<i>0.01371</i>	<i>0.04325</i>	<i>0.03689</i>	<i>0.01371</i>	<i>0.07829</i>	<i>0.03529</i>	<i>0.03023</i>	<i>0.01128</i>	<i>0.03529</i>	<i>0.03023</i>	<i>0.01128</i>
Gibbsite	-	-	-	-	-	-	-	-	-	-	-	-	-	-
HgO	-	-	-	-	-	-	-	-	-	-	-	-	-	-
KAlSiO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
La(OH) <sub>3</sub>	<i>0.00015</i>	<i>0.00007</i>	<i>0.00006</i>	<i>0.00002</i>	<i>0.00007</i>	<i>0.00006</i>	<i>0.00002</i>	<i>0.00012</i>	<i>0.00006</i>	<i>0.00005</i>	<i>0.00002</i>	<i>0.00006</i>	<i>0.00005</i>	<i>0.00002</i>
LaPO <sub>4</sub> •2H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Mn(OH) <sub>2</sub>	<i>0.11385</i>	<i>0.05180</i>	<i>0.04419</i>	<i>0.01642</i>	<i>0.05180</i>	<i>0.04419</i>	<i>0.01642</i>	<i>0.09377</i>	<i>0.04227</i>	<i>0.03620</i>	<i>0.01352</i>	<i>0.04227</i>	<i>0.03620</i>	<i>0.01352</i>
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
MnCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	<i>0.21776</i>	<i>0.09908</i>	<i>0.08452</i>	<i>0.03141</i>	<i>0.09908</i>	<i>0.08452</i>	<i>0.03141</i>	<i>0.17935</i>	<i>0.08085</i>	<i>0.06924</i>	<i>0.02585</i>	<i>0.08085</i>	<i>0.06924</i>	<i>0.02585</i>
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaAlSiO <sub>4</sub>	<i>0.52822</i>	<i>0.24034</i>	<i>0.20503</i>	<i>0.07618</i>	<i>0.24034</i>	<i>0.20503</i>	<i>0.07618</i>	<i>0.43505</i>	<i>0.19612</i>	<i>0.16797</i>	<i>0.06271</i>	<i>0.19612</i>	<i>0.16797</i>	<i>0.06271</i>
Ni(OH) <sub>2</sub>	<i>0.00462</i>	<i>0.00210</i>	<i>0.00179</i>	<i>0.00067</i>	<i>0.00210</i>	<i>0.00179</i>	<i>0.00067</i>	<i>0.00381</i>	<i>0.00172</i>	<i>0.00147</i>	<i>0.00055</i>	<i>0.00172</i>	<i>0.00147</i>	<i>0.00055</i>
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NiC <sub>2</sub> O <sub>4</sub> •2H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pb(OH) <sub>2</sub>	<i>0.00061</i>	<i>0.00028</i>	<i>0.00024</i>	<i>0.00009</i>	<i>0.00028</i>	<i>0.00024</i>	<i>0.00009</i>	<i>0.00050</i>	<i>0.00022</i>	<i>0.00019</i>	<i>0.00007</i>	<i>0.00022</i>	<i>0.00019</i>	<i>0.00007</i>
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
PbCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pu(OH) <sub>4</sub>	<i>0.00017</i>	<i>0.00008</i>	<i>0.00007</i>	<i>0.00002</i>	<i>0.00008</i>	<i>0.00007</i>	<i>0.00002</i>	<i>0.00014</i>	<i>0.00006</i>	<i>0.00005</i>	<i>0.00002</i>	<i>0.00006</i>	<i>0.00005</i>	<i>0.00002</i>
SiO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
SrCO <sub>3</sub>	<i>0.03093</i>	<i>0.01407</i>	<i>0.01201</i>	<i>0.00446</i>	<i>0.01407</i>	<i>0.01201</i>	<i>0.00446</i>	<i>0.02547</i>	<i>0.01148</i>	<i>0.00984</i>	<i>0.00367</i>	<i>0.01148</i>	<i>0.00984</i>	<i>0.00367</i>
TcO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
ZrO <sub>2</sub>	<i>0.00159</i>	<i>0.00072</i>	<i>0.00062</i>	<i>0.00023</i>	<i>0.00072</i>	<i>0.00062</i>	<i>0.00023</i>	<i>0.00131</i>	<i>0.00059</i>	<i>0.00051</i>	<i>0.00019</i>	<i>0.00059</i>	<i>0.00051</i>	<i>0.00019</i>
KNO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	<i>0.43100</i>	-	-	-	-	-	-	<i>0.35497</i>	-	-	-	-	-	-
Na <sub>2</sub> CO <sub>3</sub> •H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub> •10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> FSO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> NO <sub>3</sub> SO <sub>4</sub> •H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> •8H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> •10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>6</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF(PO <sub>4</sub> ) <sub>2</sub> •19H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaHCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>3</sub>	<i>14.02182</i>	-	-	-	-	-	-	<i>11.54846</i>	-	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> •0.25NaOH•12H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Total Volume % UDS	<i>33.58</i>	<i>8.70</i>	<i>7.42</i>	<i>2.76</i>	<i>8.70</i>	<i>7.42</i>	<i>2.76</i>	<i>27.66</i>	<i>7.10</i>	<i>6.08</i>	<i>2.27</i>	<i>7.10</i>	<i>6.08</i>	<i>2.27</i>
Solids Concentration (g/L)	<i>908.6</i>	<i>264.6</i>	<i>225.7</i>	<i>83.9</i>	<i>264.6</i>	<i>225.7</i>	<i>83.9</i>	<i>748.3</i>	<i>215.9</i>	<i>184.9</i>	<i>69.0</i>	<i>215.9</i>	<i>184.9</i>	<i>69.0</i>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Rheological Data**

Model/model Parameter	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104
Temperature (°C)	30	30	30	30	95	95	95	30	30	28	30	95	95	95
Source of Data	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031
Notes														
<b>Newtonian:</b>														
$\eta$ – Newtonian viscosity (cP)		19.449		8.501	13.678		8.307		152.942	73.090	23.286		41.731	21.367
r – correlation coefficient		0.983		0.992	0.999		1.000		0.998	0.986	0.986		0.999	1.000
<b>Ostwald (or Power Law):</b>														
m – the consistency coefficient (Pa·s <sup>-n</sup> )		1.293		0.483	0.575		0.372		1.231	8.438	0.775		4.834	1.741
n – the power-law exponent		0.283		0.308	0.361		0.351		0.652	0.187	0.404		0.187	0.247
r – correlation coefficient		0.866		0.857	0.856		0.831		0.995	0.774	0.932		0.697	0.744
<b>Bingham Plastic:</b>														
$\tau_B$ – the Bingham yield stress (Pa)		3.869		1.363	2.472		1.558		15.346	17.828	4.639		10.481	4.841
$\eta_p$ – the plastic viscosity (Pa·s)		0.008		0.004	0.006		0.004		0.112	0.021	0.010		0.011	0.007
r – correlation coefficient		0.983		0.992	0.999		1.000		0.998	0.986	0.986		0.999	1.000
<b>Herschel-Bulkley:</b>														
$\tau_0$ – the yield stress (Pa)		3.600		1.255	2.420		1.550		12.975	17.185	4.348		10.399	4.789
k – the Herschel-Bulkely consistency coefficient (Pa·s <sup>-b</sup> )		0.041		0.015	0.010		0.004		0.176	0.095	0.043		0.017	0.011
b – the Herschel-Bulkely power-law exponent		0.741		0.812	0.927		0.981		0.935	0.755	0.763		0.933	0.931
r – correlation coefficient		1.000		1.000	1.000		1.000		0.998	1.000	1.000		1.000	1.000
n/a = not applicable														

**Physical Property Data**

Physical Property	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104
Notes														
Temperature (°C)	30	30	30	30	30	30	30	30	30	30	30	30	30	30
Zeta Potential (mV)														
Bulk Density (g/mL)	1.64	1.29	1.27	1.11	1.29	1.27	1.11	1.64	1.28	1.26	1.11	1.28	1.26	1.11
vol% Settled Solids	100	n/m	n/m	n/m	n/m	n/m	n/m	100	n/m	n/m	n/m	n/m	n/m	n/m
Density of Centrifuged Solids (g/mL)	1.71	n/m	n/m	n/m	n/m	n/m	n/m	1.71	n/m	n/m	n/m	n/m	n/m	n/m
vol% Centrifuged Solids	82.5	n/m	n/m	n/m	n/m	n/m	n/m	100	n/m	n/m	n/m	n/m	n/m	n/m
wt% Centrifuged Solids	86.1	n/m	n/m	n/m	n/m	n/m	n/m	100	n/m	n/m	n/m	n/m	n/m	n/m
Supernatant Density (g/mL)	1.28	1.12	1.12	1.05	1.12	1.12	1.05	1.28	1.14	1.14	1.06	1.14	1.14	1.06
Density of Settled Solids (g/mL)	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% Settled Supernatant	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% dissolved solids in supernatant	40.59	35.66	35.66	33.35	35.66	35.66	33.35	40.59	36.30	36.30	33.65	36.30	36.30	33.65
wt% total solids in Centrifuged Sludge	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% Total Solids	62.3	n/m	n/m	n/m	n/m	n/m	n/m	67.7	n/m	n/m	n/m	n/m	n/m	n/m
wt% UDS	55.40	20.49	17.82	7.58	20.49	17.82	7.58	45.63	16.88	14.68	6.24	16.88	14.68	6.24
Density of Solids (g/cc)	2.71	3.04	3.04	3.04	3.04	3.04	3.04	2.71	3.04	3.04	3.04	3.04	3.04	3.04

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

Settling Data

Settling Schedule	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104
Notes:		C04-012		C04-012							C04-013			
Temperature (°C)	30	30	30	30	95	95	95	30	30	30	30	95	95	95
Total initial volume		100		100							100			
5 minutes														
10 minutes														
15 minutes														
20 minutes														
30 minutes														
40 minutes														
50 minutes														
1 hour														
2 hours		99		92								95		
3 hours														
4 hours														
5 hours		97		81								93		
6 hours														
24 hours		92		68								85		
32 hours		90		64								83		
48 hours		90		62								82		
56 hours		89												
72 hours final settled														

Shear Strength Data

Shear Strength Schedule	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104	S-104
Source of Data	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031	WHC-SD-WM-DP-031
Notes:	Page C04-006									Page C04-006				
Temperature (°C)	Unspecified									Unspecified				
Description	Shear Vane at unspecified gel time or temperature									Shear Vane at unspecified gel time or temperature				
Gelation Time/Shear Strength (Pa)														
5 minutes														
10 minutes														
15 minutes														
20 minutes														
30 minutes														
40 minutes														
50 minutes														
1 hour														
2 hours														
3 hours														
4 hours														
5 hours														
6 hours														
24 hours														
32 hours														
48 hours														
56 hours														
72 hours	1040									6380				
Infinte time (GRE)														

## 241-S-112

Analyte/Sample	S-112	S-112	S-112	S-112	S-112	S-112
Description	V1L/V2L; decanted Saltcake supernate after 1st contact with water at 50C	V1L/V2L; decanted Saltcake supernate after 1st contact with water at 50C	V1L/V2L; decanted Saltcake supernate after 1st contact with water at 50C	V1SV2S; decanted Saltcake supernate after 2nd contact with water at 50C	V1SV2S; decanted Saltcake supernate after 2nd contact with water at 50C	V1SV2S; decanted Saltcake supernate after 2nd contact with water at 50C
Model Basis	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free	Salt Free
Report No./Source of Data	RPP-10984 Rev. 0	RPP-10984 Rev. 0	RPP-10984 Rev. 0	RPP-10984 Rev. 0	RPP-10984 Rev. 0	RPP-10984 Rev. 0

## Rheological Data

Model/model Parameter	S-112	S-112	S-112	S-112	S-112	S-112
Temperature (°C)	20	35	50	20	35	50
Source of Data	RPP-10984 Rev. 0	RPP-10984 Rev. 0	RPP-10984 Rev. 0	RPP-10984 Rev. 0	RPP-10984 Rev. 0	RPP-10984 Rev. 0
Notes	Table 3-17	Table 3-17	Table 3-17	Table 3-17	Table 3-17	Table 3-17
<b>Newtonian:</b>						
$\eta$ – Newtonian viscosity (cP)	5.700	4.000	2.900	2.000	1.800	1.400
r – correlation coefficient						
<b>Ostwald (or Power Law):</b>						
m – the consistency coefficient (Pa·s <sup>n</sup> )						
n – the power-law exponent						
r – correlation coefficient						
<b>Bingham Plastic:</b>						
$\tau_B$ - the Bingham yield stress (Pa)	0.000	0.000	0.000	0.000	0.000	0.000
$\eta_p$ - the plastic viscosity (Pa·s)	<i>0.006</i>	<i>0.004</i>	<i>0.003</i>	<i>0.002</i>	<i>0.002</i>	<i>0.001</i>
r – correlation coefficient						
<b>Herschel-Bulkley:</b>						
$\tau_H$ - the yield stress (Pa)						
k - the Herschel-Bulkely consistency coefficient (Pa·s <sup>b</sup> )						
b - the Herschel-Bulkely power-law exponent						
r – correlation coefficient						
n/a = not applicable						

## Physical Property Data

Physical Property	S-112	S-112	S-112	S-112	S-112	S-112
<b>Notes</b>						
Temperature (°C)	50	50	50	50	50	50
Zeta Potential (mV)	n/m	n/m	n/m	n/m	n/m	n/m
Bulk Density (g/mL)	1.36	1.36	1.36	1.15	1.15	1.15
vol% Settled Solids	n/m	n/m	n/m	n/m	n/m	n/m
Density of Centrifuged Solids (g/mL)	n/m	n/m	n/m	n/m	n/m	n/m
vol% Centrifuged Solids	n/m	n/m	n/m	n/m	n/m	n/m
wt% Centrifuged Solids	n/m	n/m	n/m	n/m	n/m	n/m
Supernatant Density (g/mL)	<i>1.36</i>	<i>1.36</i>	<i>1.36</i>	1.16	1.16	1.16
Density of Settled Solids (g/mL)	n/m	n/m	n/m	n/m	n/m	n/m
wt% Settled Supernatant	n/m	n/m	n/m	n/m	n/m	n/m
wt% dissolved solids in supernatant	n/m	n/m	n/m	n/m	n/m	n/m
wt% total solids in Centrifuged Sludge	n/m	n/m	n/m	n/m	n/m	n/m
wt% Total Solids	n/m	n/m	n/m	n/m	n/m	n/m
wt% UDS	0.00	0.00	0.00	0.00	0.00	0.00
Density of Solids (g/cc)	<i>3.02</i>	<i>3.02</i>	<i>3.02</i>	<i>3.02</i>	<i>3.02</i>	<i>3.02</i>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

Model Chemical Data From ESP

Analyte/Sample	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101
Description	Initial Slurry	Window C Segment 4	Window C Segment 4	Window C Segment 4	Window C Segment 4	Window C Segment 8	Window C Segment 8	Window C Segment 8	Window C Segment 8	Window C Segment 13	Window C Segment 13	Window C Segment 13	Window C Segment 15	Window C Segment 15	Window C Segment 15
Model Basis	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty
Report No/Source of Data	HNF-1666 Rev 0A, HNF-1666 Rev 0B	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394
<b>Solid Phases (vol% of bulk)</b>															
(NaAlO <sub>2</sub> ) <sub>2</sub> ·2.5H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Bi <sub>2</sub> O <sub>3</sub>	<i>0.00035</i>	<i>0.00045</i>	<i>0.00052</i>	<i>0.00057</i>	<i>0.00045</i>	<i>0.00047</i>	<i>0.00059</i>	<i>0.00047</i>	<i>0.00032</i>	<i>0.00006</i>	<i>0.00019</i>	<i>0.00025</i>	<i>0.00037</i>	<i>0.00129</i>	<i>0.00092</i>
BiOCl	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Boehmite	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca <sub>3</sub> OH(PO <sub>3</sub> ) <sub>3</sub>	<i>0.01535</i>	<i>0.01976</i>	<i>0.02258</i>	<i>0.02486</i>	<i>0.01976</i>	<i>0.02042</i>	<i>0.02596</i>	<i>0.02065</i>	<i>0.01411</i>	<i>0.00282</i>	<i>0.00838</i>	<i>0.01105</i>	<i>0.01607</i>	<i>0.05668</i>	<i>0.04041</i>
CaC <sub>2</sub> O <sub>4</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaF <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CrOOH	<i>0.15259</i>	<i>0.19641</i>	<i>0.22447</i>	<i>0.24720</i>	<i>0.19641</i>	<i>0.20298</i>	<i>0.25810</i>	<i>0.20527</i>	<i>0.14030</i>	<i>0.02806</i>	<i>0.08328</i>	<i>0.10987</i>	<i>0.15974</i>	<i>0.56352</i>	<i>0.40171</i>
FeOOH	<i>0.01375</i>	<i>0.01770</i>	<i>0.02023</i>	<i>0.02228</i>	<i>0.01770</i>	<i>0.01829</i>	<i>0.02326</i>	<i>0.01850</i>	<i>0.01264</i>	<i>0.00253</i>	<i>0.00751</i>	<i>0.00990</i>	<i>0.01440</i>	<i>0.05078</i>	<i>0.03620</i>
Gibbsite	<i>2.98106</i>	<i>3.83716</i>	<i>4.38532</i>	<i>4.82930</i>	<i>3.83716</i>	<i>3.96549</i>	<i>5.04227</i>	<i>4.01019</i>	<i>2.74083</i>	<i>0.54817</i>	<i>1.62695</i>	<i>2.14636</i>	<i>3.12067</i>	<i>11.00893</i>	<i>7.84784</i>
HgO	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
KAlSiO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
La(OH) <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
LaPO <sub>4</sub> ·2H <sub>2</sub> O	<i>0.00034</i>	<i>0.00043</i>	<i>0.00049</i>	<i>0.00054</i>	<i>0.00043</i>	<i>0.00045</i>	<i>0.00057</i>	<i>0.00045</i>	<i>0.00031</i>	<i>0.00006</i>	<i>0.00018</i>	<i>0.00024</i>	<i>0.00035</i>	<i>0.00124</i>	<i>0.00088</i>
Mn(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
MnCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> U <sub>2</sub> O <sub>7</sub>	<i>0.00205</i>	<i>0.00264</i>	<i>0.00302</i>	<i>0.00333</i>	<i>0.00264</i>	<i>0.00273</i>	<i>0.00347</i>	<i>0.00276</i>	<i>0.00189</i>	<i>0.00038</i>	<i>0.00112</i>	<i>0.00148</i>	<i>0.00215</i>	<i>0.00758</i>	<i>0.00540</i>
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaAlSiO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ni(OH) <sub>2</sub>	<i>0.00580</i>	<i>0.00746</i>	<i>0.00853</i>	<i>0.00939</i>	<i>0.00746</i>	<i>0.00771</i>	<i>0.00981</i>	<i>0.00780</i>	<i>0.00533</i>	<i>0.00107</i>	<i>0.00316</i>	<i>0.00417</i>	<i>0.00607</i>	<i>0.02141</i>	<i>0.01526</i>
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NiC <sub>2</sub> O <sub>4</sub> ·2H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pb(OH) <sub>2</sub>	<i>0.00180</i>	<i>0.00232</i>	<i>0.00265</i>	<i>0.00292</i>	<i>0.00232</i>	<i>0.00240</i>	<i>0.00305</i>	<i>0.00243</i>	<i>0.00166</i>	<i>0.00033</i>	<i>0.00098</i>	<i>0.00130</i>	<i>0.00189</i>	<i>0.00666</i>	<i>0.00475</i>
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
PbCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pu(OH) <sub>4</sub>	<i>0.00000</i>	<i>0.00001</i>	<i>0.00001</i>	<i>0.00001</i>	<i>0.00001</i>	<i>0.00001</i>	<i>0.00001</i>	<i>0.00001</i>	<i>0.00000</i>	<i>0.00000</i>	<i>0.00000</i>	<i>0.00000</i>	<i>0.00000</i>	<i>0.00002</i>	<i>0.00001</i>
SiO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
SrCO <sub>3</sub>	<i>0.00030</i>	<i>0.00038</i>	<i>0.00044</i>	<i>0.00048</i>	<i>0.00038</i>	<i>0.00039</i>	<i>0.00050</i>	<i>0.00040</i>	<i>0.00027</i>	<i>0.00005</i>	<i>0.00016</i>	<i>0.00021</i>	<i>0.00031</i>	<i>0.00109</i>	<i>0.00078</i>
TcO <sub>2</sub>	<i>0.00002</i>	<i>0.00002</i>	<i>0.00002</i>	<i>0.00003</i>	<i>0.00002</i>	<i>0.00002</i>	<i>0.00003</i>	<i>0.00002</i>	<i>0.00001</i>	<i>0.00000</i>	<i>0.00001</i>	<i>0.00001</i>	<i>0.00002</i>	<i>0.00006</i>	<i>0.00004</i>
ZrO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
KNO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	<i>1.76726</i>	<i>2.27477</i>	<i>2.59974</i>	<i>2.86294</i>	<i>2.27477</i>	<i>2.35085</i>	<i>2.98920</i>	<i>2.37736</i>	<i>1.62484</i>	<i>0.32497</i>	<i>0.96450</i>	<i>1.27242</i>	<i>1.85002</i>	<i>6.52640</i>	<i>4.65242</i>
Na <sub>2</sub> CO <sub>3</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> FSO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> NO <sub>3</sub> SO <sub>3</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> ·8H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>6</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF(PO <sub>3</sub> ) <sub>2</sub> ·19H <sub>2</sub> O	<i>0.14709</i>	<i>0.18933</i>	<i>0.21637</i>	<i>0.23828</i>	<i>0.18933</i>	<i>0.19566</i>	<i>0.24879</i>	<i>0.19786</i>	<i>0.13523</i>	<i>0.02705</i>	<i>0.08027</i>	<i>0.10590</i>	<i>0.15397</i>	<i>0.54318</i>	<i>0.38721</i>
NaHCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> ·0.25NaOH·12H <sub>2</sub> O	<i>0.77865</i>	<i>1.00226</i>	<i>1.14544</i>	<i>1.26141</i>	<i>1.00226</i>	<i>1.03578</i>	<i>1.31704</i>	<i>1.04746</i>	<i>0.71590</i>	<i>0.14318</i>	<i>0.42496</i>	<i>0.56063</i>	<i>0.81512</i>	<i>2.87552</i>	<i>2.04985</i>
Total Volume % UDS	<i>5.87</i>	<i>7.55</i>	<i>8.63</i>	<i>9.50</i>	<i>7.55</i>	<i>7.80</i>	<i>9.92</i>	<i>7.89</i>	<i>5.39</i>	<i>1.08</i>	<i>3.20</i>	<i>4.22</i>	<i>6.14</i>	<i>21.66</i>	<i>15.44</i>
Solids Concentration (g/L)	<b>138.3</b>	<b>178.0</b>	<b>203.4</b>	<b>224.0</b>	<b>178.0</b>	<b>183.9</b>	<b>233.9</b>	<b>186.0</b>	<b>127.1</b>	<b>25.4</b>	<b>75.5</b>	<b>99.6</b>	<b>144.7</b>	<b>510.6</b>	<b>364.0</b>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.



**Rheological Data**

Model/model Parameter	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101
Temperature (°C)	25	32	50	65	80	32	50	65	80	32	50	65	80	
Source of Data	HNF-1666 Rev 0A, HNF-1666 Rev 0B	WHC-EP-0628	WHC-EP-0628	WHC-EP-0628	WHC-EP-0628	WHC-EP-0628	WHC-EP-0628	WHC-EP-0628	WHC-EP-0628	WHC-EP-0628	WHC-EP-0628	WHC-EP-0628	WHC-EP-0628	
Notes	Table 3-2													
<b>Newtonian:</b>														
$\eta$ - Newtonian viscosity (cP)	n/m	61.51	25.67	16.40	12.42	55.16	30.00	7.76	5.51	45.59	21.20	14.18	12.49	
r - correlation coefficient	n/m	1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00	
<b>Ostwald (or Power Law):</b>														
m - the consistency coefficient (Pas <sup>n</sup> )	n/m	0.07	0.04	0.04	0.02	0.05	0.05	0.25	0.78	0.04	0.03	0.02	0.02	
n - the power-law exponent	n/m	0.97	0.92	0.85	0.89	1.03	0.93	0.01	0.11	1.02	0.92	0.93	0.89	
r - correlation coefficient	n/m	1.00	1.00	1.00	1.00	1.00	1.00	0.15	0.43	1.00	1.00	1.00	1.00	
<b>Bingham Plastic:</b>														
$\tau_B$ - the Bingham yield stress (Pa)	n/m	0.36	0.30	0.30	0.27	0.26	0.25	0.00	0.00	0.30	0.28	0.23	0.21	
$\eta_p$ - the plastic viscosity (Pas)	n/m	0.060	0.025	0.015	0.012	0.054	0.029	0.008	0.005	0.045	0.020	0.013	0.012	
r - correlation coefficient	n/m	1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00	
<b>Herschel-Bulkley:</b>														
$\tau_0$ - the yield stress (Pa)	n/m	0.00	0.06	0.06	0.06	0.06	0.06	0.05	0.08	0.06	0.06	0.05	0.05	
k - the Herschel-Bulkley consistency coefficient (Pa·s <sup>n</sup> )	n/m	0.07	0.04	0.04	0.02	0.04	0.04	0.003	0.003	0.04	0.03	0.02	0.02	
b - the Herschel-Bulkley power-law exponent	n/m	0.98	0.93	0.86	0.91	1.04	0.94	1.13	1.08	1.04	0.93	0.95	0.90	
r - correlation coefficient	n/m	1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00	
n/a = not applicable														

**Physical Property Data**

Physical Property	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101
Notes														
Temperature (°C)	25	32	50	65	80	32	50	65	80	32	50	65	80	
Zeta Potential (mV)														
Bulk Density (g/mL)	1.40	1.50	1.51	1.50	1.50	1.53	1.54	1.54	1.48	1.44	1.45	1.45	1.44	1.67
vol% Settled Solids	n/m	60	60	58	51	44	48	54	56	39	37	39	40	100
Density of Centrifuged Solids (g/mL)	n/m	2.1	1.9	1.9	1.9	1.93	1.85	1.82	2.16	2.1	2.1	2	2.2	1.74
vol% Centrifuged Solids	n/m	5	7	7	7	22	23	20	8	7	7	7	6	84
wt% Centrifuged Solids	n/m	10	9	9	9	28	27	24	10	11	10	9	8	88
Supernatant Density (g/mL)	1.34	1.43	1.43	1.41	1.43	1.46	1.45	1.47	1.43	1.43	1.42	1.41	1.38	1.48
Density of Settled Solids (g/mL)	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% Settled Supernatant	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% dissolved solids in supernatant	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% total solids in Centrifuged Sludge	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% Total Solids	n/m	60.6	60.6	60.6	60.6	61.1	61.1	61.1	61.1	65	65	65	65	71.6
wt% UDS	9.91	11.87	13.47	14.93	11.87	12.02	15.19	12.08	8.59	1.77	5.20	6.87	10.05	30.58
Density of Solids (g/cc)	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.36

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Shear Strength Data**

Shear Strength Schedule	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	
Source of Data	<i>HNF-1666 Rev 0A, HNF-1666 Rev 0B</i>														WHC-EP-0628	WHC-EP-0628
Notes:	HNF-1666 Rev. 0B															
Temperature (°C)															32	50
Description	Sample S99T000529; several months undisturbed														Sample 066 Stored at 222-S	Sample 066 Stored at 222-S
Gelation Time/Shear Strength (Pa)																
5 minutes																
10 minutes																
15 minutes																
20 minutes																
30 minutes																
40 minutes																
50 minutes																
1 hour																
2 hours																
3 hours																
4 hours																
5 hours																
6 hours																
24 hours																
32 hours																
48 hours																
56 hours																
72 hours	13036														4750	730
Infinite time (GRE)																

## Model Chemical Data Fro

Analyte/Sample	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	
Description	Window C Segment 15	Window C Segment 15	Window C Segment 19	Window C Segment 19	Window C Segment 19	Window C Segment 19	Window C Segment 19	Window C Segment 22	Window C Segment 22	Window C Segment 22	Window C Segment 22	Auger R-9221 Crust	Auger R-9221 Crust	Auger R-9221 Crust	Auger R-9221 Crust	Window E Segment 3
Model Basis	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty
Report No./Source of Data	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394	WHC-EP-0628 PNL-MITS2394	WHC-SD-WM-DTR-026
Solid Phases (vol% of bulk)																
(NaAlO <sub>2</sub> ) <sub>2</sub> ·2.5H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Bi <sub>2</sub> O <sub>3</sub>	0.00139	0.00081	0.00125	0.00133	0.00143	0.00195	0.00166	0.00141	0.00136	0.00123	0.00254	0.00260	0.00254	0.00254	0.00076	
BiOCl	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Boehmite	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca <sub>3</sub> OH(PO <sub>4</sub> ) <sub>3</sub>	0.06106	0.03566	0.05495	0.05833	0.06277	0.08559	0.07292	0.06178	0.05939	0.05378	0.11130	0.11386	0.11130	0.11130	0.03319	
CaC <sub>2</sub> O <sub>4</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaF <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CrOOH	0.60702	0.35455	0.54632	0.57995	0.62403	0.85096	0.72494	0.61419	0.59045	0.53468	1.10655	1.13201	1.10655	1.10655	0.33001	
FeOOH	0.05470	0.03195	0.04923	0.05226	0.05624	0.07669	0.06533	0.05535	0.05321	0.04819	0.09972	0.10202	0.09972	0.09972	0.02974	
Gibbsite	11.85878	6.92643	10.67290	11.32997	12.19115	16.62429	14.16246	11.99878	11.53503	10.44561	21.61758	22.11499	21.61758	21.61758	6.44710	
HgO	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
KAlSiO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
La(OH) <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
LaPO <sub>4</sub> ·2H <sub>2</sub> O	0.00133	0.00078	0.00120	0.00128	0.00137	0.00187	0.00159	0.00135	0.00130	0.00118	0.00243	0.00249	0.00243	0.00243	0.00073	
Mn(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
MnCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> U <sub>2</sub> O <sub>7</sub>	0.00817	0.00477	0.00735	0.00780	0.00839	0.01145	0.00975	0.00826	0.00794	0.00719	0.01488	0.01523	0.01488	0.01488	0.00444	
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaAlSiO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ni(OH) <sub>2</sub>	0.02306	0.01347	0.02076	0.02204	0.02371	0.03233	0.02754	0.02334	0.02243	0.02032	0.04204	0.04301	0.04204	0.04204	0.01254	
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NiC <sub>2</sub> O <sub>4</sub> ·2H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pb(OH) <sub>2</sub>	0.00718	0.00419	0.00646	0.00686	0.00738	0.01006	0.00857	0.00726	0.00698	0.00632	0.01308	0.01338	0.01308	0.01308	0.00390	
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
PbCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pu(OH) <sub>4</sub>	0.00002	0.00001	0.00001	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00001	0.00003	0.00003	0.00003	0.00001	
SiO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
SrCO <sub>3</sub>	0.00118	0.00069	0.00106	0.00113	0.00121	0.00165	0.00141	0.00119	0.00115	0.00104	0.00215	0.00220	0.00215	0.00215	0.00064	
TcO <sub>2</sub>	0.00006	0.00004	0.00006	0.00006	0.00007	0.00009	0.00008	0.00006	0.00006	0.00006	0.00012	0.00012	0.00012	0.00012	0.00003	
ZrO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
KNO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	7.03021	4.10618	6.32719	6.71672	7.22725	9.85535	8.39590	7.11321	6.83829	6.19245	12.81551	13.11038	12.81551	12.81551	3.82202	
Na <sub>2</sub> CO <sub>3</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> FSO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> NO <sub>3</sub> ·SO <sub>3</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> ·8H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>4</sub> (SO <sub>3</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF(PO <sub>3</sub> ) <sub>2</sub> ·19H <sub>2</sub> O	0.58511	0.34175	0.52660	0.55902	0.60151	0.82024	0.69878	0.59202	0.56914	0.51539	1.06661	1.09116	1.06661	1.06661	0.31810	
NaHCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> ·0.25NaOH·12H <sub>2</sub> O	3.09750	1.80917	2.78775	2.95937	3.18431	4.34224	3.69922	3.13407	3.01293	2.72838	5.64648	5.77641	5.64648	5.64648	1.68397	
Total Volume % UDS	23.34	13.63	21.00	22.30	23.99	32.71	27.87	23.61	22.70	20.56	42.54	43.52	42.54	42.54	12.69	
Solids Concentration (g/L)	550.1	321.3	495.0	525.5	565.5	771.1	656.9	556.5	535.0	484.5	1,002.7	1,025.8	1,002.7	1,002.7	299.0	

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Rheological Data**

<b>Model/model Parameter</b>															
Temperature (°C)															
<b>Source of Data</b>															
Notes															
<b>Newtonian:</b>															
$\eta$ - Newtonian viscosity (cP)															
r - correlation coefficient															
<b>Ostwald (or Power Law):</b>															
m - the consistency coefficient (Pa·s <sup>n</sup> )															
n - the power-law exponent															
r - correlation coefficient															
<b>Bingham Plastic:</b>															
$\tau_B$ - the Bingham yield stress (Pa)															
$\eta_p$ - the plastic viscosity (Pa·s)															
r - correlation coefficient															
<b>Herschel-Bulkley:</b>															
$\tau_0$ - the yield stress (Pa)															
k - the Herschel-Bulkely consistency coefficient (Pa·s <sup>b</sup> )															
b - the Herschel-Bulkely power-law exponent															
r - correlation coefficient															
n/a = not applicable															

**Physical Property Data**

Physical Property	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101
Notes															
Temperature (°C)	65	80	32	50	65	80	32	50	65	80	28	50	65	80	32
Zeta Potential (mV)															
Bulk Density (g/mL)	1.70	1.66	1.68	1.66	1.66	1.74	1.71	1.71	1.71	1.70	1.77	1.78	1.77	1.77	1.60
vol% Settled Solids	100	98	100	100	100	100	100	100	100	99	100	100	100	100	71
Density of Centrifuged Solids (g/mL)	1.76	1.79	1.75	1.75	1.73	1.9	1.78	1.82	1.79	1.79	1.82	1.82	1.81	1.82	1.8
vol% Centrifuged Solids	75	69	78	72	65	62	79	73	68	64	96	96	96	95	35
wt% Centrifuged Solids	78	74	79	76	67	68	83	78	72	68	99	99	99	99	40
Supernatant Density (g/mL)	1.50	1.55	1.50	1.46	1.44	1.44	1.46	1.51	1.52	1.53	<i>1.34</i>	<i>1.34</i>	<i>1.34</i>	<i>1.34</i>	1.49
Density of Settled Solids (g/mL)	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% Settled Supernatant	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% dissolved solids in supernatant	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% total solids in Centrifuged Sludge	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% Total Solids	71.6	71.6	68.6	68.6	68.6	68.6	71.5	71.5	71.5	71.5	85.7	85.7	85.7	85.7	n/m
wt% UDS	<i>32.36</i>	<i>19.35</i>	<i>29.47</i>	<i>31.66</i>	<i>34.06</i>	<i>44.32</i>	<i>38.42</i>	<i>32.55</i>	<i>31.29</i>	<i>28.50</i>	<i>56.65</i>	<i>57.63</i>	<i>56.65</i>	<i>56.65</i>	<i>18.69</i>
Density of Solids (g/cc)	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.36

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Shear Strength Data**

Shear Strength Schedule	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>
Source of Data	WHC-EP-0628	WHC-EP-0628	WHC-EP-0628	WHC-EP-0628	WHC-EP-0628	WHC-EP-0628	WHC-EP-0628	WHC-EP-0628	WHC-EP-0628	WHC-EP-0628	WHC-EP-0628	WHC-EP-0628	WHC-EP-0628	WHC-EP-0628	WHC-SD-WM-DRT-026
Notes:															
Temperature (°C)	65	80	32	50	65	80	32	50	65	80	28	50	65	80	32
Description	Sample 066 Stored at 222-S	Sample 066 Stored at 222-S	Sample 019 Stored at 222-S	Sample 019 Stored at 222-S	Sample 019 Stored at 222-S	Sample 019 Stored at 222-S	Sample 067 Stored at 222-S	Sample 067 Stored at 222-S	Sample 067 Stored at 222-S	Sample 067 Stored at 222-S	Sample 817 Stored at 222-S	Sample 817 Stored at 222-S	Sample 817 Stored at 222-S	Sample 817 Stored at 222-S	Sample 1229 Stored at 222-S
Gelation Time/Shear Strength (Pa)															
5 minutes															
10 minutes															
15 minutes															
20 minutes															
30 minutes															
40 minutes															
50 minutes															
1 hour															
2 hours															
3 hours															
4 hours															
5 hours															
6 hours															
24 hours															
32 hours															
48 hours															
56 hours															
72 hours	2100	530	1500	640	300	510	11600	2640	400	1400	25000	4200	210	270	500
Infinite time (GRE)															

## Model Chemical Data Fro

Analyte/Sample	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	
Description	Window E Segment 15	Window E Segment 15	Window E Segment 15	Window E Segment 15	Window E Segment 19	Window E Segment 19	Window E Segment 19	Window E Segment 19	Window E Segment 19	in-situ	in-situ	in-situ	in-situ	in-situ	Window C Segment 16	Window C Segment 16R	Window E Segment 18
Model Basis	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty
Report No/Source of Data	WHC-SD-WM-DTR-026	WHC-SD-WM-DTR-026	WHC-SD-WM-DTR-026	WHC-SD-WM-DTR-026	WHC-SD-WM-DTR-026	WHC-SD-WM-DTR-026	WHC-SD-WM-DTR-026	WHC-SD-WM-DTR-026	WHC-SD-WM-DTR-026	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	PNNL-10198	PNNL-10198	PNNL-10198
Solid Phases (vol% of bulk)																	
(NaAlO <sub>2</sub> ) <sub>2</sub> •2.5H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Bi <sub>2</sub> O <sub>3</sub>	0.00074	0.00092	0.00071	0.00076	0.00114	0.00169	0.00146	0.00143	0.00102	0.00204	0.00204	0.00204	0.00204	0.00204	0.00131	0.00131	0.00131
BiOCl	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Boehmite	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca <sub>3</sub> OH(PO <sub>3</sub> ) <sub>3</sub>	0.03242	0.04016	0.03126	0.03319	0.04987	0.07413	0.06405	0.06252	0.04490	0.08961	0.08961	0.08961	0.08961	0.08961	0.05733	0.05733	0.05733
CaC <sub>2</sub> O <sub>4</sub> •H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaF <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CrOOH	0.32231	0.39922	0.31076	0.33001	0.49576	0.73702	0.63674	0.62153	0.44637	0.89095	0.89095	0.89095	0.89095	0.89095	0.57002	0.57002	0.57002
FeOOH	0.02905	0.03598	0.02801	0.02974	0.04468	0.06642	0.05738	0.05601	0.04023	0.08029	0.08029	0.08029	0.08029	0.08029	0.05137	0.05137	0.05137
Gibbsite	6.29675	7.79921	6.07107	6.44710	9.68515	14.39854	12.43937	12.14214	8.72035	17.40560	17.40560	17.40560	17.40560	17.40560	11.13590	11.13590	11.13590
HgO	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
KAlSiO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
La(OH) <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
LaPO <sub>4</sub> •2H <sub>2</sub> O	0.00071	0.00088	0.00068	0.00073	0.00109	0.00162	0.00140	0.00137	0.00098	0.00196	0.00196	0.00196	0.00196	0.00196	0.00125	0.00125	0.00125
Mn(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
MnCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	0.00434	0.00537	0.00418	0.00444	0.00667	0.00991	0.00856	0.00836	0.00600	0.01198	0.01198	0.01198	0.01198	0.01198	0.00767	0.00767	0.00767
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaAlSiO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ni(OH) <sub>2</sub>	0.01225	0.01517	0.01181	0.01254	0.01884	0.02800	0.02419	0.02362	0.01696	0.03385	0.03385	0.03385	0.03385	0.03385	0.02166	0.02166	0.02166
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NiC <sub>2</sub> O <sub>4</sub> •2H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pb(OH) <sub>2</sub>	0.00381	0.00472	0.00367	0.00390	0.00586	0.00871	0.00753	0.00735	0.00528	0.01053	0.01053	0.01053	0.01053	0.01053	0.00674	0.00674	0.00674
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
PbCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pu(OH) <sub>3</sub>	0.00001	0.00001	0.00001	0.00001	0.00001	0.00002	0.00002	0.00002	0.00001	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002
SiO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
SrCO <sub>3</sub>	0.00063	0.00078	0.00060	0.00064	0.00096	0.00143	0.00124	0.00121	0.00087	0.00173	0.00173	0.00173	0.00173	0.00173	0.00111	0.00111	0.00111
TcO <sub>2</sub>	0.00003	0.00004	0.00003	0.00003	0.00005	0.00008	0.00007	0.00006	0.00005	0.00009	0.00009	0.00009	0.00009	0.00009	0.00006	0.00006	0.00006
ZrO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
KNO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	3.73289	4.62359	3.59910	3.82202	5.74163	8.53586	7.37440	7.19820	5.16967	10.31853	10.31853	10.31853	10.31853	10.31853	6.60167	6.60167	6.60167
Na <sub>2</sub> CO <sub>3</sub> •H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub> •10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> FSO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> NO <sub>2</sub> SO <sub>4</sub> •H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> •8H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> •10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>4</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF(PO <sub>3</sub> ) <sub>2</sub> •19H <sub>2</sub> O	0.31068	0.38481	0.29955	0.31810	0.47787	0.71043	0.61376	0.59909	0.43026	0.85879	0.85879	0.85879	0.85879	0.85879	0.54945	0.54945	0.54945
NaHCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> PO <sub>3</sub> •0.25NaOH•12H <sub>2</sub> O	1.64470	2.03714	1.58575	1.68397	2.52975	3.76088	3.24915	3.17151	2.27774	4.54632	4.54632	4.54632	4.54632	4.54632	2.90868	2.90868	2.90868
Total Volume % UDS	12.39	15.35	11.95	12.69	19.06	28.33	24.48	23.89	17.16	34.25	34.25	34.25	34.25	34.25	21.91	21.91	21.91
Solids Concentration (g/L)	<b>292.1</b>	<b>361.8</b>	<b>281.6</b>	<b>299.0</b>	<b>449.2</b>	<b>667.9</b>	<b>577.0</b>	<b>563.2</b>	<b>404.5</b>	<b>807.3</b>	<b>807.3</b>	<b>807.3</b>	<b>807.3</b>	<b>807.3</b>	<b>516.5</b>	<b>516.5</b>	<b>516.5</b>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Rheological Data**

Model/model Parameter																
Temperature (°C)																
Source of Data																
Notes																
<b>Newtonian:</b>																
$\eta$ - Newtonian viscosity (cP)																
r - correlation coefficient																
<b>Ostwald (or Power Law):</b>																
m - the consistency coefficient (Pa·s <sup>n</sup> )																
n - the power-law exponent																
r - correlation coefficient																
<b>Bingham Plastic:</b>																
$\tau_B$ - the Bingham yield stress (Pa)																
$\eta_p$ - the plastic viscosity (Pa·s)																
r - correlation coefficient																
<b>Herschel-Bulkley:</b>																
$\tau_{sp}$ - the yield stress (Pa)																
k - the Herschel-Bulkely consistency coefficient (Pa·s <sup>b</sup> )																
b - the Herschel-Bulkely power-law exponent																
r - correlation coefficient																
n/a = not applicable																

**Physical Property Data**

Physical Property	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101
Notes																
Temperature (°C)	32	50	65	80	32	50	65	80						50	50	50
Zeta Potential (mV)																
Bulk Density (g/mL)	1.65	1.64	1.62	1.60	1.72	1.75	1.74	1.72	1.63	1.78	1.78	1.78	1.78	1.68	1.68	1.68
vol% Settled Solids	94	95	90	92	100	95	100	100	100	100	100	100	100	100	100	100
Density of Centrifuged Solids (g/mL)	1.72	1.78	1.74	1.82	1.76	1.82	1.84	1.85	<i>1.86</i>	<i>1.86</i>	<i>1.86</i>	<i>1.86</i>	<i>1.86</i>	1.75	1.75	1.75
vol% Centrifuged Solids	60	48	43	33	78	73	63	57	<i>73.7</i>	<i>73.7</i>	<i>73.7</i>	<i>73.7</i>	<i>73.7</i>	76	76	76
wt% Centrifuged Solids	63	51	46	37	80	77	67	62	<i>77.3</i>	<i>77.3</i>	<i>77.3</i>	<i>77.3</i>	<i>77.3</i>	80	80	80
Supernatant Density (g/mL)	1.55	1.51	1.52	1.49	1.57	1.51	1.54	1.52	<i>1.48</i>	<i>1.48</i>	<i>1.48</i>	<i>1.48</i>	<i>1.48</i>	1.49	1.49	1.49
Density of Settled Solids (g/mL)	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m						n/m	n/m	n/m
wt% Settled Supernatant	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m						n/m	n/m	n/m
wt% dissolved solids in supernatant	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m						n/m	n/m	n/m
wt% total solids in Centrifuged Sludge	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m						n/m	n/m	n/m
wt% Total Solids	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m						n/m	n/m	n/m
wt% UDS	<i>17.70</i>	<i>22.06</i>	<i>17.38</i>	<i>18.69</i>	<i>26.12</i>	<i>38.16</i>	<i>33.16</i>	<i>32.74</i>	<i>24.81</i>	<i>45.36</i>	<i>45.36</i>	<i>45.36</i>	<i>45.36</i>	<i>30.75</i>	<i>30.75</i>	<i>30.75</i>
Density of Solids (g/cc)	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.36

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

Shear Strength Data

Shear Strength Schedule	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-103</i>	<i>SY-103</i>	<i>SY-103</i>	<i>SY-103</i>	<i>SY-103</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>
Source of Data	WHC-EP0628	WHC-EP0628	WHC-EP0628	WHC-EP0628	WHC-EP0628	WHC-EP0628	WHC-EP0628	WHC-EP0628	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	PNL-10198	PNL-10198	PNL-10198
Notes:									Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer			
Temperature (°C)	32	50	65	80	32	50	65	80	47	47	47	47	46	50	50	50
Description	Sample 818 Stored at 222-S	Sample 818 Stored at 222-S	Sample 818 Stored at 222-S	Sample 818 Stored at 222-S	Sample 1223 Stored at 222-S	Sample 1223 Stored at 222-S	Sample 1223 Stored at 222-S	Sample 1223 Stored at 222-S	Riser 4A Loosely Settled Solids Depth from bottom of tank is 75 cm	Riser 4A Loosely Settled Solids Depth from bottom of tank is 57 cm	Riser 4A Loosely Settled Solids Depth from bottom of tank is 45 cm	Riser 4A Loosely Settled Solids Depth from bottom of tank is 37 cm	Riser 4A Loosely Settled Solids Depth from bottom of tank is 16 cm	Window C Segment 16 Homogenized	Window C Segment 16R Homogenized	Window C Segment 18 Homogenized
Gelation Time/Shear Strength (Pa)																
5 minutes																
10 minutes																
15 minutes																
20 minutes																
30 minutes																
40 minutes																
50 minutes																
1 hour																
2 hours																
3 hours																
4 hours																
5 hours																
6 hours																
24 hours																
32 hours																
48 hours																
56 hours																
72 hours	1720	450	790	230	1850	370	730	670	0.77	11	17	20	28	240	330	190
Infinte time (GRE)																



Model Chemical Data Fro

Analyte/Sample	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101
Description	Window C Segment 16, 16R, & 18 Composite	Window C Segment 16, 16R, & 18 Composite	Window C Segment 16, 16R, & 18 Composite	Window C Segment 16, 16R, & 18 Composite	Window C Segment 16, 16R, & 18 Composite	Window C Segment 16, 16R, & 18 Composite	Window C Segment 16, 16R, & 18 Composite	Window C Segment 16, 16R, & 18 Composite	Window C Segment 16, 16R, & 18 Composite	Window C Segment 16, 16R, & 18 Composite	Window C Segment 16, 16R, & 18 Composite	Window C Segment 16, 16R, & 18 Composite	Window C Segment 16, 16R, & 18 Composite	Window C Segment 16, 16R, & 18 Composite	Window C Segment 16, 16R, & 18 Composite
Model Basis	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Washed	Washed	Washed	Washed	Washed
Report No./Source of Data	PNNL-10198	PNNL-10198	PNNL-10198	PNNL-10198	PNNL-10198	PNNL-10198	PNNL-10198	PNNL-10198	PNNL-10198	PNNL-10198	PNNL-10198	PNNL-10198	PNNL-10198	PNNL-10198	PNNL-10198
Solid Phases (vol% of bulk)															
(NaAlO <sub>2</sub> ) <sub>2</sub> ·2.5H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Bi <sub>2</sub> O <sub>3</sub>	0.00158	0.00083	0.00049	0.00125	0.00047	0.00007	0.00063	0.00014	0.00007	0.00010	(0.00040)	(0.00050)	0.00043	(0.00009)	(0.00071)
BiOCl	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Boehmite	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ca <sub>3</sub> OH(PO <sub>3</sub> ) <sub>3</sub>	0.06940	0.03621	0.02162	0.05495	0.02042	0.00305	0.02780	0.00633	0.00305	0.00438	(0.01734)	(0.02188)	0.01881	(0.00379)	(0.03107)
CaC <sub>2</sub> O <sub>4</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CaF <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CrOOH	0.69002	0.36001	0.21497	0.54632	0.20298	0.03035	0.27638	0.06290	0.03035	0.04350	(0.17243)	(0.21749)	0.18703	(0.03770)	(0.30886)
FeOOH	0.06218	0.03244	0.01937	0.04923	0.01829	0.00274	0.02491	0.00567	0.00274	0.00392	(0.01554)	(0.01960)	0.01686	(0.00340)	(0.02783)
Gibbsite	13.48030	7.03320	4.19957	10.67290	3.96549	0.59294	5.39945	1.22890	0.59294	0.84977	(3.36859)	(4.24883)	3.65388	(0.73650)	(6.03396)
HgO	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
KAlSiO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
La(OH) <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
LaPO <sub>4</sub> ·2H <sub>2</sub> O	0.00152	0.00079	0.00047	0.00120	0.00045	0.00007	0.00061	0.00014	0.00007	0.00010	(0.00038)	(0.00048)	0.00041	(0.00008)	(0.00068)
Mn(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
MnCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> U <sub>2</sub> O <sub>7</sub>	0.00928	0.00484	0.00289	0.00735	0.00273	0.00041	0.00372	0.00085	0.00041	0.00059	(0.00232)	(0.00293)	0.00252	(0.00051)	(0.00415)
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaAlSiO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Ni(OH) <sub>2</sub>	0.02622	0.01368	0.00817	0.02076	0.00771	0.00115	0.01050	0.00239	0.00115	0.00165	(0.00655)	(0.00826)	0.00711	(0.00143)	(0.01174)
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NiC <sub>2</sub> O <sub>4</sub> ·2H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pb(OH) <sub>2</sub>	0.00816	0.00426	0.00254	0.00646	0.00240	0.00036	0.00327	0.00074	0.00036	0.00051	(0.00204)	(0.00257)	0.00221	(0.00045)	(0.00365)
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
PbCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Pu(OH) <sub>4</sub>	0.00002	0.00001	0.00001	0.00001	0.00001	0.00000	0.00001	0.00000	0.00000	0.00000	(0.00000)	(0.00001)	0.00001	(0.00000)	(0.00001)
SiO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
SrCO <sub>3</sub>	0.00134	0.00070	0.00042	0.00106	0.00039	0.00006	0.00054	0.00012	0.00006	0.00008	(0.00033)	(0.00042)	0.00036	(0.00007)	(0.00060)
TcO <sub>2</sub>	0.00007	0.00004	0.00002	0.00006	0.00002	0.00000	0.00003	0.00001	0.00000	0.00000	(0.00002)	(0.00002)	0.00002	(0.00000)	(0.00003)
ZrO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
KNO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	7.99150	4.16948	2.48963	6.32719	2.35085	0.35151	3.20095	0.72852	0.35151	-	-	-	-	-	-
Na <sub>2</sub> CO <sub>3</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> FSO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> NO <sub>3</sub> ·SO <sub>3</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> ·8H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>6</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaF(PO <sub>3</sub> ) <sub>2</sub> ·19H <sub>2</sub> O	0.66512	0.34702	0.20721	0.52660	0.19566	0.02926	0.26641	0.06063	0.02926	-	-	-	-	-	-
NaHCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
NaNO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> ·0.25NaOH·12H <sub>2</sub> O	3.52104	1.83706	1.09692	2.78775	1.03578	0.15487	1.41033	0.32099	0.15487	-	-	-	-	-	-
Total Volume % UDS	26.53	13.84	8.26	21.00	7.80	1.17	10.63	2.42	1.17	0.90	(3.59)	(4.52)	3.89	(0.78)	(6.42)
Solids Concentration (g/L)	625.3	326.2	194.8	495.0	183.9	27.5	250.4	57.0	27.5	23.3	(92.4)	(116.5)	100.2	(20.2)	(165.4)

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Rheological Data**

Model/model Parameter	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101
Temperature (°C)	50	70	90	50	70	90	50	70	90	50	70	90	50	70	90
Source of Data	PNNL-10198	PNNL-10198	PNNL-10198	PNNL-10198	PNNL-10198	PNNL-10198	PNNL-10198	PNNL-10198	PNNL-10198	PNNL-10198	PNNL-10198	PNNL-10198	PNNL-10198	PNNL-10198	PNNL-10198
<b>Notes</b>															
<b>Newtonian:</b>															
$\eta$ - Newtonian viscosity (cP)	96.92	74.24	72.35	89.47	61.90	27.16	30.43	31.68	26.33	17.46	15.70	9.70	7.46	7.75	3.86
r - correlation coefficient	1.00	1.00	0.99	1.00	1.00	0.99	1.00	1.00	0.99	1.00	1.00	1.00	1.00	1.00	1.00
<b>Ostwald (or Power Law):</b>															
m - the consistency coefficient (Pas <sup>n</sup> )	0.64	0.76	2.12	0.36	0.92	0.63	0.32	0.34	0.52	0.08	0.22	0.15	0.09	0.14	0.04
n - the power-law exponent	0.68	0.60	0.42	0.76	0.54	0.46	0.60	0.60	0.49	0.75	0.55	0.53	0.57	0.51	0.59
r - correlation coefficient	0.99	0.99	0.98	1.00	0.99	0.97	0.99	0.99	0.98	0.99	0.97	0.98	0.98	0.97	0.98
<b>Bingham Plastic:</b>															
$\tau_B$ - the Bingham yield stress (Pa)	5.07	5.08	8.15	3.39	5.20	2.68	1.31	2.17	2.63	0.71	1.29	0.81	0.57	0.70	0.27
$\eta_p$ - the plastic viscosity (Pas)	0.082	0.059	0.048	0.079	0.046	0.019	0.027	0.025	0.018	0.015	0.012	0.007	0.006	0.006	0.003
r - correlation coefficient	1.00	1.00	0.99	1.00	1.00	0.99	1.00	1.00	0.99	1.00	1.00	1.00	1.00	1.00	1.00
<b>Herschel-Bulkley:</b>															
$\tau_0$ - the yield stress (Pa)	4.12	4.35	6.09	2.65	4.04	2.32	1.02	1.59	2.06	0.46	1.26	0.71	0.51	0.65	0.26
k - the Herschel-Bulkely consistency coefficient (Pa·s <sup>n</sup> )	0.15	0.11	0.28	0.13	0.15	0.049	0.047	0.074	0.073	0.033	0.013	0.014	0.010	0.009	0.003
b - the Herschel-Bulkely power-law exponent	0.90	0.90	0.72	0.92	0.81	0.85	0.91	0.83	0.78	0.88	0.98	0.89	0.91	0.93	0.98
r - correlation coefficient	1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00	0.99	1.00	1.00	1.00	1.00	1.00
n/a = not applicable															

**Physical Property Data**

Physical Property	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101	SY-101
Notes	Centrifuged Solids are Filtered Solids	Centrifuged Solids are Filtered Solids	Centrifuged Solids are Filtered Solids	Centrifuged Solids are Filtered Solids	Centrifuged Solids are Filtered Solids	Centrifuged Solids are Filtered Solids	Centrifuged Solids are Filtered Solids	Centrifuged Solids are Filtered Solids	Centrifuged Solids are Filtered Solids	Centrifuged Solids are Filtered Solids	Centrifuged Solids are Filtered Solids	Centrifuged Solids are Filtered Solids	Centrifuged Solids are Filtered Solids	Centrifuged Solids are Filtered Solids	Centrifuged Solids are Filtered Solids
Temperature (°C)	50	70	90	50	70	90	50	70	90	50	70	90	50	70	90
Zeta Potential (mV)															
Bulk Density (g/mL)	1.72	1.61	1.58	1.68	1.53	1.51	1.60	1.55	1.51	1.48	1.42	1.42	1.34	1.29	1.25
vol% Settled Solids	100	100	100	100	98	96	96	99	98	89	n/m	76	34	34	33
Density of Centrifuged Solids (g/mL)	1.74	1.7	1.74	1.68	1.61	1.66	1.73	1.86	1.7	1.7	1.72	1.68	1.92	1.65	1.93
vol% Centrifuged Solids															
wt% Centrifuged Solids	83	71	66	60	61	49	68	67	59	40	38	42	25	24	24
Supernatant Density (g/mL)	1.49	1.49	1.51	1.50	1.46	1.50	1.51	1.53	1.50	1.47	1.46	1.47	1.29	1.30	1.33
Density of Settled Solids (g/mL)	1.72	1.63	1.58	1.68	1.51	1.51	1.59	1.57	1.51	1.51	n/m	1.42	1.42	1.38	1.25
wt% Settled Supernatant	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% dissolved solids in supernatant	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% total solids in Centrifuged Sludge	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% Total Solids	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m	n/m
wt% UDS	36.35	20.26	12.33	29.47	12.02	1.82	15.65	3.68	1.82	1.57	-6.50	-8.20	7.48	-1.57	-13.23
Density of Solids (g/cc)	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.36	2.58	2.58	2.58	2.58	2.58	2.58

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Shear Strength Data**

Shear Strength Schedule	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>	<i>SY-101</i>
Source of Data	PNL-10198	PNL-10198	PNL-10198	PNL-10198	PNL-10198	PNL-10198	PNL-10198	PNL-10198	PNL-10198	PNL-10198	PNL-10198	PNL-10198	PNL-10198	PNL-10198	PNL-10198
Notes:															
Temperature (°C)	50			50			50	50	50	50	50	50	50	50	50
Description	Window C Segment 16, 16R, & 18 Composite			Window C Composite 10% Dilution											
Gelation Time/Shear Strength (Pa)															
5 minutes															
10 minutes															
15 minutes															
20 minutes															
30 minutes															
40 minutes															
50 minutes															
1 hour															
2 hours															
3 hours															
4 hours															
5 hours															
6 hours															
24 hours															
32 hours															
48 hours															
56 hours															
72 hours	60			110											
Infinite time (GRE)															

## Model Chemical Data From ESP

Analyte\Sample	SY-102	SY-102	SY-102
Description	Undiluted	1% Dilution with NaNO3	48% Dilution with 1M NaNO3
Model Basis	Salty	Salty	Salt Free
Report No/Source of Data	PNNL-11352	PNNL-11352	PNNL-11352
Solid Phases (vol% of bulk)			
(NaAlO <sub>2</sub> ) <sub>2</sub> •2.5H <sub>2</sub> O	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	-	-	-
Bi <sub>2</sub> O <sub>3</sub>	<i>0.12803</i>	<i>0.12504</i>	<i>0.04863</i>
BiOCl	-	-	-
Boehmite	-	-	-
Ca(OH) <sub>2</sub>	-	-	-
Ca <sub>3</sub> OH(PO <sub>4</sub> ) <sub>3</sub>	<i>0.37952</i>	<i>0.37067</i>	<i>0.14416</i>
CaC <sub>2</sub> O <sub>4</sub> •H <sub>2</sub> O	-	-	-
CaCO <sub>3</sub>	-	-	-
CaF <sub>2</sub>	-	-	-
CrOOH	<i>1.49365</i>	<i>1.45881</i>	<i>0.56734</i>
FeOOH	<i>1.03054</i>	<i>1.00650</i>	<i>0.39144</i>
Gibbsite	<i>25.37101</i>	<i>24.77916</i>	<i>9.63684</i>
H <sub>2</sub> O	-	-	-
KAlSiO <sub>4</sub>	-	-	-
La(OH) <sub>3</sub>	-	-	-
LaPO <sub>4</sub> •2H <sub>2</sub> O	<i>0.01280</i>	<i>0.01250</i>	<i>0.00486</i>
Mn(OH) <sub>2</sub>	<i>0.17399</i>	<i>0.16994</i>	<i>0.06609</i>
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-
MnCO <sub>3</sub>	-	-	-
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	<i>0.05988</i>	<i>0.05848</i>	<i>0.02274</i>
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	-	-	-
NaAlSiO <sub>4</sub>	-	-	-
Ni(OH) <sub>2</sub>	<i>0.04675</i>	<i>0.04566</i>	<i>0.01776</i>
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-
NiC <sub>2</sub> O <sub>4</sub> •2H <sub>2</sub> O	-	-	-
Pb(OH) <sub>2</sub>	<i>0.03699</i>	<i>0.03613</i>	<i>0.01405</i>
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-
PbCO <sub>3</sub>	-	-	-
Pu(OH) <sub>4</sub>	<i>0.00504</i>	<i>0.00492</i>	<i>0.00191</i>
SiO <sub>2</sub>	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-
SrCO <sub>3</sub>	<i>0.00791</i>	<i>0.00773</i>	<i>0.00301</i>
TcO <sub>2</sub>	<i>0.00018</i>	<i>0.00017</i>	<i>0.00007</i>
ZrO <sub>2</sub>	<i>0.00173</i>	<i>0.00169</i>	<i>0.00066</i>
KNO <sub>3</sub>	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	<i>8.07249</i>	<i>7.88417</i>	-
Na <sub>2</sub> CO <sub>3</sub> •H <sub>2</sub> O	-	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-	-
Na <sub>2</sub> SO <sub>4</sub> •10H <sub>2</sub> O	-	-	-
Na <sub>3</sub> FSO <sub>4</sub>	-	-	-
Na <sub>3</sub> NO <sub>3</sub> SO <sub>4</sub> •H <sub>2</sub> O	-	-	-
Na <sub>3</sub> PO <sub>4</sub> •8H <sub>2</sub> O	-	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> •10H <sub>2</sub> O	-	-	-
Na <sub>6</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-	-
NaF	-	-	-
NaF(PO <sub>4</sub> ) <sub>2</sub> •19H <sub>2</sub> O	<i>3.09380</i>	<i>3.02163</i>	-
NaHCO <sub>3</sub>	-	-	-
NaNO <sub>2</sub>	-	-	-
NaNO <sub>3</sub>	-	-	-
Na <sub>3</sub> PO <sub>4</sub> •0.25NaOH•12H <sub>2</sub> O	<i>3.94679</i>	<i>3.85472</i>	-
Total Volume % UDS	<i>43.86</i>	<i>42.84</i>	<i>10.92</i>
Solids Concentration (g/L)	<b>1,081.4</b>	<b>1,056.2</b>	<b>294.2</b>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

## Rheological Data

Model/model Parameter	<i>SY-102</i>	<i>SY-102</i>	<i>SY-102</i>
Temperature (°C)	25	25	25
Source of Data	<i>PNNL-11352</i>	<i>PNNL-11352</i>	<i>PNNL-11352</i>
Notes	Page 2.8	Page 2.8	Page 2.8
<b>Newtonian:</b>			
$\eta$ – Newtonian viscosity (cP)	16.725	16.022	0.893
r – correlation coefficient	0.959	0.991	0.980
<b>Ostwald (or Power Law):</b>			
m – the consistency coefficient (Pa·s <sup>-n</sup> )	1.764	1.188	0.003
n – the power-law exponent	0.135	0.201	0.782
r – correlation coefficient	0.929	0.915	0.992
<b>Bingham Plastic:</b>			
$\tau_B$ - the Bingham yield stress (Pa)	2.602	2.120	0.010
$\eta_p$ - the plastic viscosity (Pa·s)	0.005	0.006	0.001
r – correlation coefficient	0.959	0.991	0.980
<b>Herschel-Bulkley:</b>			
$\tau_H$ - the yield stress (Pa)	2.377	1.882	0.000
k - the Herschel-Bulkely consistency coefficient (Pa·s <sup>-b</sup> )	0.039	0.038	0.003
b - the Herschel-Bulkely power-law exponent	0.647	0.699	0.785
r – correlation coefficient	0.975	0.989	0.992
n/a = not applicable			

## Physical Property Data

Physical Property	<i>SY-102</i>	<i>SY-102</i>	<i>SY-102</i>
	Letter Report-1990 RD Scheele		
Notes	PNNL-11352		
Temperature (°C)	25	25	25
Zeta Potential (mV)	-37		
Bulk Density (g/mL)	1.80	<i>1.79</i>	<i>1.30</i>
vol% Settled Solids	100	n/m	n/m
Density of Centrifuged Solids (g/mL)	1.83	n/m	n/m
vol% Centrifuged Solids	92	n/m	n/m
wt% Centrifuged Solids	93.93	n/m	n/m
Supernatant Density (g/mL)	1.28	<i>1.28</i>	<i>1.13</i>
Density of Settled Solids (g/mL)	n/m	n/m	n/m
wt% Settled Supernatant	n/m	n/m	n/m
wt% dissolved solids in supernatant	n/m	n/m	n/m
wt% total solids in Centrifuged Sludge	n/m	n/m	n/m
wt% Total Solids	67.3	n/m	n/m
wt% UDS	<i>60.08</i>	<i>59.14</i>	<i>22.61</i>
Density of Solids (g/cc)	<i>2.47</i>	<i>2.47</i>	<i>2.69</i>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Shear Strength Data**

Shear Strength Schedule	<i>SY-102</i>		
Source of Data	<i>PNNL-11352</i>		
Notes:	reference of DiCenso et al. 1995		
Temperature (°C)			
Description	Page 2.11		
Gelation Time/Shear Strength (Pa)			
5 minutes			
10 minutes			
15 minutes			
20 minutes			
30 minutes			
40 minutes			
50 minutes			
1 hour			
2 hours			
3 hours			
4 hours			
5 hours			
6 hours			
24 hours			
32 hours			
48 hours			
56 hours			
72 hours	3900		
Infinte time (GRE)			

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

## Model Chemical Data From ESP

Analyte/Sample	SY-103	SY-103	SY-103	SY-103	SY-103	SY-103	SY-103	SY-103	SY-103	SY-103
Description	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ	in-situ
Model Basis	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty	Salty
Source of Data	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296
Solid Phases (vol% of bulk)										
(NaAlO <sub>2</sub> ) <sub>2</sub> ·2.5H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-
Bi <sub>2</sub> O <sub>3</sub>	0.00119	0.00119	0.00119	0.00119	0.00119	0.00119	0.00119	0.00119	0.00119	0.00119
BiOCl	-	-	-	-	-	-	-	-	-	-
Boehmite	-	-	-	-	-	-	-	-	-	-
Ca(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-
Ca <sub>5</sub> OH(PO <sub>4</sub> ) <sub>3</sub>	0.05816	0.05816	0.05816	0.05816	0.05816	0.05816	0.05816	0.05816	0.05816	0.05816
CaC <sub>2</sub> O <sub>4</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-
CaCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-
CaF <sub>2</sub>	-	-	-	-	-	-	-	-	-	-
CrOOH	0.25879	0.25879	0.25879	0.25879	0.25879	0.25879	0.25879	0.25879	0.25879	0.25879
FeOOH	0.11237	0.11237	0.11237	0.11237	0.11237	0.11237	0.11237	0.11237	0.11237	0.11237
Gibbsite	5.49441	5.49441	5.49441	5.49441	5.49441	5.49441	5.49441	5.49441	5.49441	5.49441
HgO	-	-	-	-	-	-	-	-	-	-
KAlSiO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-
La(OH) <sub>3</sub>	-	-	-	-	-	-	-	-	-	-
LaPO <sub>4</sub> ·2H <sub>2</sub> O	0.00158	0.00158	0.00158	0.00158	0.00158	0.00158	0.00158	0.00158	0.00158	0.00158
Mn(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-
MnCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	0.02192	0.02192	0.02192	0.02192	0.02192	0.02192	0.02192	0.02192	0.02192	0.02192
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-
NaAlSiO <sub>4</sub>	0.28376	0.28376	0.28376	0.28376	0.28376	0.28376	0.28376	0.28376	0.28376	0.28376
Ni(OH) <sub>2</sub>	0.00641	0.00641	0.00641	0.00641	0.00641	0.00641	0.00641	0.00641	0.00641	0.00641
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-
NiC <sub>2</sub> O <sub>4</sub> ·2H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-
Pb(OH) <sub>2</sub>	0.00514	0.00514	0.00514	0.00514	0.00514	0.00514	0.00514	0.00514	0.00514	0.00514
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-
PbCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-
Pu(OH) <sub>4</sub>	0.00003	0.00003	0.00003	0.00003	0.00003	0.00003	0.00003	0.00003	0.00003	0.00003
SiO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-	-
SrCO <sub>3</sub>	0.00031	0.00031	0.00031	0.00031	0.00031	0.00031	0.00031	0.00031	0.00031	0.00031
TcO <sub>2</sub>	0.00006	0.00006	0.00006	0.00006	0.00006	0.00006	0.00006	0.00006	0.00006	0.00006
ZrO <sub>2</sub>	0.00119	0.00119	0.00119	0.00119	0.00119	0.00119	0.00119	0.00119	0.00119	0.00119
KNO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	1.78840	1.78840	1.78840	1.78840	1.78840	1.78840	1.78840	1.78840	1.78840	1.78840
Na <sub>2</sub> CO <sub>3</sub> ·H <sub>2</sub> O	0.68236	0.68236	0.68236	0.68236	0.68236	0.68236	0.68236	0.68236	0.68236	0.68236
Na <sub>2</sub> SO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> FSO <sub>4</sub>	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> NO <sub>3</sub> SO <sub>3</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> ·8H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-
Na <sub>6</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	0.51162	0.51162	0.51162	0.51162	0.51162	0.51162	0.51162	0.51162	0.51162	0.51162
NaF	-	-	-	-	-	-	-	-	-	-
NaF(PO <sub>4</sub> ) <sub>2</sub> ·19H <sub>2</sub> O	2.96922	2.96922	2.96922	2.96922	2.96922	2.96922	2.96922	2.96922	2.96922	2.96922
NaHCO <sub>3</sub>	-	-	-	-	-	-	-	-	-	-
NaNO <sub>2</sub>	-	-	-	-	-	-	-	-	-	-
NaNO <sub>3</sub>	6.45015	6.45015	6.45015	6.45015	6.45015	6.45015	6.45015	6.45015	6.45015	6.45015
Na <sub>3</sub> PO <sub>4</sub> ·0.25NaOH·12H <sub>2</sub> O	-	-	-	-	-	-	-	-	-	-
Total Volume % UDS	18.65	18.65	18.65	18.65	18.65	18.65	18.65	18.65	18.65	18.65
Solids Concentration (g/L)	431.1	431.1	431.1	431.1	431.1	431.1	431.1	431.1	431.1	431.1

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Physical Property Data**

Physical Property	<i>SY-103</i>	<i>SY-103</i>	<i>SY-103</i>	<i>SY-103</i>	<i>SY-103</i>	<i>SY-103</i>	<i>SY-103</i>	<i>SY-103</i>	<i>SY-103</i>	<i>SY-103</i>
Source of Data										
Temperature (°C)										
Zeta Potential (mV)										
Bulk Density (g/mL)	1.57	1.57	1.57	1.57	1.57	1.57	1.57	1.57	1.57	1.57
vol% Settled Solids										
Density of Centrifuged Solids (g/mL)										
vol% Centrifuged Solids										
wt% Centrifuged Solids										
Supernatant Density (g/mL)	1.40	1.40	1.40	1.40	1.40	1.40	1.40	1.40	1.40	1.40
Density of Settled Solids (g/mL)										
wt% Settled Supernatant										
wt% dissolved solids in supernatant										
wt% total solids in Centrifuged Sludge										
wt% Total Solids	27.46	27.46	27.46	27.46	27.46	27.46	27.46	27.46	27.46	27.46
wt% UDS	2.31	2.31	2.31	2.31	2.31	2.31	2.31	2.31	2.31	2.31
Density of Solids (g/cc)										

**Shear Strength Data**

Shear Strength Schedule	<i>SY-103</i>	<i>SY-103</i>	<i>SY-103</i>	<i>SY-103</i>	<i>SY-103</i>	<i>SY-103</i>	<i>SY-103</i>	<i>SY-103</i>	<i>SY-103</i>	<i>SY-103</i>
Source of Data	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296	RPP-6655 PNNL-11296
Instrumentation	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer
Temperature (°C)	35	37	38	38	37	35	37	38	38	37
Description	Riser 17C Depth from bottom of tank is 300 cm	Riser 17C Depth from bottom of tank is 250 cm	Riser 17C Depth from bottom of tank is 200 cm	Riser 17C Depth from bottom of tank is 150 cm	Riser 17C Depth from bottom of tank is 100 cm	Riser 22A Depth from bottom of tank is 300 cm	Riser 22A Depth from bottom of tank is 250 cm	Riser 22A Depth from bottom of tank is 200 cm	Riser 22A Depth from bottom of tank is 150 cm	Riser 22A Depth from bottom of tank is 100 cm
Gelation Time/Shear Strength (Pa)										
5 minutes										
10 minutes										
15 minutes										
20 minutes										
30 minutes										
40 minutes										
50 minutes										
1 hour										
2 hours										
3 hours										
4 hours										
5 hours										
6 hours										
24 hours										
32 hours										
48 hours										
56 hours										
72 hours										
infinte time (GRE)	10	45	95	155	228	48	118	180	242	295

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.



## Model Chemical Data From ESP

Analyte/Sample	T-102 Core 55	T-102 Core 55	T-102 Core 55	T-102 Core 55
Description	Segment 2 1:1 dilution	Segment 2 3:1 dilution	Segment 2 1:1 dilution	Segment 2 3:1 dilution
Model Basis	Salt Free	Salt Free	Salt Free	Salt Free
Report No/Source of Data	HNF-SD-WM-ER-700 Rev. 0 WHC-SD-WM-DP-052 Rev 0	HNF-SD-WM-ER-700 Rev. 0 WHC-SD-WM-DP-052 Rev 0	HNF-SD-WM-ER-700 Rev. 0 WHC-SD-WM-DP-052 Rev 0	HNF-SD-WM-ER-700 Rev. 0 WHC-SD-WM-DP-052 Rev 0
Solid Phases (vol% of bulk)				
(NaAlO <sub>2</sub> ) <sub>2</sub> •2.5H <sub>2</sub> O	-	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	<i>0.00083</i>	<i>0.00037</i>	<i>0.00083</i>	<i>0.00037</i>
Bi <sub>2</sub> O <sub>3</sub>	<i>0.00292</i>	<i>0.00129</i>	<i>0.00292</i>	<i>0.00129</i>
BiOCl	-	-	-	-
Boehmite	-	-	-	-
Ca(OH) <sub>2</sub>	-	-	-	-
Ca <sub>5</sub> (OH)(PO <sub>4</sub> ) <sub>3</sub>	<i>0.00901</i>	<i>0.00399</i>	<i>0.00901</i>	<i>0.00399</i>
CaC <sub>2</sub> O <sub>4</sub> •H <sub>2</sub> O	-	-	-	-
CaCO <sub>3</sub>	-	-	-	-
CaF <sub>2</sub>	-	-	-	-
CrOOH	<i>0.00011</i>	<i>0.00005</i>	<i>0.00011</i>	<i>0.00005</i>
FeOOH	<i>0.07697</i>	<i>0.03408</i>	<i>0.07697</i>	<i>0.03408</i>
Gibbsite	<i>4.13662</i>	<i>1.83152</i>	<i>4.13662</i>	<i>1.83152</i>
HgO	-	-	-	-
KAlSiO <sub>4</sub>	-	-	-	-
La(OH) <sub>3</sub>	-	-	-	-
LaPO <sub>4</sub> •2H <sub>2</sub> O	<i>0.00042</i>	<i>0.00019</i>	<i>0.00042</i>	<i>0.00019</i>
Mn(OH) <sub>2</sub>	-	-	-	-
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	<i>0.00897</i>	<i>0.00397</i>	<i>0.00897</i>	<i>0.00397</i>
MnCO <sub>3</sub>	-	-	-	-
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	<i>0.02984</i>	<i>0.01321</i>	<i>0.02984</i>	<i>0.01321</i>
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	<i>0.33528</i>	<i>0.14845</i>	<i>0.33528</i>	<i>0.14845</i>
NaAlSiO <sub>4</sub>	<i>0.07256</i>	<i>0.03213</i>	<i>0.07256</i>	<i>0.03213</i>
Ni(OH) <sub>2</sub>	<i>0.00048</i>	<i>0.00021</i>	<i>0.00048</i>	<i>0.00021</i>
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-
NiC <sub>2</sub> O <sub>4</sub> •2H <sub>2</sub> O	-	-	-	-
Pb(OH) <sub>2</sub>	<i>0.00122</i>	<i>0.00054</i>	<i>0.00122</i>	<i>0.00054</i>
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-
PbCO <sub>3</sub>	-	-	-	-
Pu(OH) <sub>4</sub>	<i>0.00001</i>	<i>0.00000</i>	<i>0.00001</i>	<i>0.00000</i>
SiO <sub>2</sub>	-	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-
SrCO <sub>3</sub>	<i>0.00018</i>	<i>0.00008</i>	<i>0.00018</i>	<i>0.00008</i>
TcO <sub>2</sub>	-	-	-	-
ZrO <sub>2</sub>	<i>0.00015</i>	<i>0.00007</i>	<i>0.00015</i>	<i>0.00007</i>
KNO <sub>3</sub>	-	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	-	-	-	-
Na <sub>2</sub> CO <sub>3</sub> •H <sub>2</sub> O	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub> •10H <sub>2</sub> O	-	-	-	-
Na <sub>3</sub> FSO <sub>4</sub>	-	-	-	-
Na <sub>3</sub> NO <sub>3</sub> SO <sub>4</sub> •H <sub>2</sub> O	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> •8H <sub>2</sub> O	-	-	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> •10H <sub>2</sub> O	-	-	-	-
Na <sub>6</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-	-	-
NaF	-	-	-	-
NaF(PO <sub>4</sub> ) <sub>2</sub> •19H <sub>2</sub> O	-	-	-	-
NaHCO <sub>3</sub>	-	-	-	-
NaNO <sub>2</sub>	-	-	-	-
NaNO <sub>3</sub>	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> •0.25NaOH•12H <sub>2</sub> O	-	-	-	-
Total Volume % UDS	<i>4.68</i>	<i>2.07</i>	<i>4.68</i>	<i>2.07</i>
Solids Concentration (g/L)	<b>116.1</b>	<b>51.4</b>	<b>116.1</b>	<b>51.4</b>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

## Rheological Data

Model/model Parameter	T-102	T-102	T-102	T-102
Temperature (°C)	30	30	90	90
Source of Data	<i>HNF-SD-WM-ER-700</i> Rev. 0 <i>WHC-SD-WM-DP-052</i> Rev 0	<i>HNF-SD-WM-ER-700</i> Rev. 0 <i>WHC-SD-WM-DP-052</i> Rev 0	<i>HNF-SD-WM-ER-700</i> Rev. 0 <i>WHC-SD-WM-DP-052</i> Rev 0	<i>HNF-SD-WM-ER-700</i> Rev. 0 <i>WHC-SD-WM-DP-052</i> Rev 0
Notes	Taylor Vorticies observed fit over 0-20 1/sec	Taylor Vorticies observed fit over 0-80 1/sec	Taylor Vorticies observed fit over 0-12 1/sec	Taylor Vorticies observed fit over 0-20 1/sec
<b>Newtonian:</b>				
$\eta$ – Newtonian viscosity (cP)	1.840	1.167	1.130	1.154
r – correlation coefficient	0.988	1.000	0.831	0.375
<b>Ostwald (or Power Law):</b>				
m – the consistency coefficient (Pa·s <sup>-n</sup> )	0.003	0.002	0.008	0.010
n – the power-law exponent	0.804	0.817	0.172	0.001
r – correlation coefficient	0.960	0.992	0.997	1.000
<b>Bingham Plastic:</b>				
$\tau_B$ – the Bingham yield stress (Pa)	0.009	0.010	0.003	0.009
$\eta_p$ – the plastic viscosity (Pa·s)	0.001	0.001	0.001	0.000
r – correlation coefficient	0.988	1.000	0.831	0.375
<b>Herschel-Bulkley:</b>				
$\tau_H$ – the yield stress (Pa)	0.009	0.007	0.001	0.007
k – the Herschel-Bulkely consistency coefficient (Pa·s <sup>-b</sup> )	0.001	0.002	0.005	0.003
b – the Hershel-Bulkely power-law exponent	0.994	0.908	0.313	0.008
r – correlation coefficient	0.987	0.998	0.993	1.000
n/a = not applicable				

## Physical Property Data

Physical Property	T-102	T-102	T-102	T-102
Notes				
Temperature (°C)	30	30	30	30
Zeta Potential (mV)				
Bulk Density (g/mL)	1.11	1.05	1.11	1.05
vol% Settled Solids	15.7	8.3	15.7	8.3
Density of Centrifuged Solids (g/mL)	n/m	n/m	n/m	n/m
vol% Centrifuged Solids	n/m	n/m	n/m	n/m
wt% Centrifuged Solids	n/m	n/m	n/m	n/m
Supernatant Density (g/mL)	<i>1.04</i>	<i>1.02</i>	<i>1.04</i>	<i>1.02</i>
Density of Settled Solids (g/mL)	n/m	n/m	n/m	n/m
wt% Settled Supernatant	n/m	n/m	n/m	n/m
wt% dissolved solids in supernatant	<i>21.72</i>	<i>21.25</i>	<i>21.72</i>	<i>21.25</i>
wt% total solids in Centrifuged Sludge	n/m	n/m	n/m	n/m
wt% Total Solids	n/m	n/m	n/m	n/m
wt% UDS	<i>10.46</i>	<i>4.90</i>	<i>10.46</i>	<i>4.90</i>
Density of Solids (g/cc)	<i>2.48</i>	<i>2.48</i>	<i>2.48</i>	<i>2.48</i>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Settling Data**

Settling Schedule	<i>T-102</i>	<i>T-102</i>		
Notes:	WHC-SD-WM-DP-052 C08-19	WHC-SD-WM-DP-052 C08-24		
Temperature (°C)	25	25		
Total initial volume	100	100		
5 minutes				
10 minutes				
15 minutes				
20 minutes				
30 minutes				
40 minutes				
50 minutes				
1 hour				
2 hours	18	11		
3 hours				
4 hours				
5 hours	17	10		
6 hours	17	10		
24 hours	17			
32 hours	17			
48 hours				
56 hours				
72 hours final settled				

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

## Model Chemical Data From ESP

Analyte/Sample	T-107	T-107	T-107	T-107	T-107
Description	no dilution	1:1 dilution	3:1 dilution	1:1 dilution	3:1 dilution
Model Basis	Salty	Salt Free	Salt Free	Salt Free	Salt Free
Report No./Source of Data	WHC-SD-WM-ER-382, rev 0	WHC-SD-WM-ER-382, rev 0	WHC-SD-WM-ER-382, rev 0	WHC-SD-WM-ER-382, rev 0	WHC-SD-WM-ER-382, rev 0
Solid Phases (vol% of bulk)					
(NaAlO <sub>2</sub> ) <sub>2</sub> •2.5H <sub>2</sub> O	-	-	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	<i>0.00008</i>	<i>0.00008</i>	<i>0.00004</i>	<i>0.00008</i>	<i>0.00004</i>
Bi <sub>2</sub> O <sub>3</sub>	<i>0.11961</i>	<i>0.12696</i>	<i>0.05809</i>	<i>0.12696</i>	<i>0.05809</i>
BiOCl	-	-	-	-	-
Boehmite	-	-	-	-	-
Ca(OH) <sub>2</sub>	-	-	-	-	-
Ca <sub>2</sub> OH(PO <sub>4</sub> ) <sub>3</sub>	-	-	-	-	-
CaC <sub>2</sub> O <sub>4</sub> •H <sub>2</sub> O	-	-	-	-	-
CaCO <sub>3</sub>	-	-	-	-	-
CaF <sub>2</sub>	<i>0.11698</i>	<i>0.12417</i>	<i>0.05682</i>	<i>0.12417</i>	<i>0.05682</i>
CrOOH	<i>0.01187</i>	<i>0.01260</i>	<i>0.00576</i>	<i>0.01260</i>	<i>0.00576</i>
FeOOH	<i>1.04158</i>	<i>1.10564</i>	<i>0.50589</i>	<i>1.10564</i>	<i>0.50589</i>
Gibbsite	<i>3.22914</i>	<i>3.42773</i>	<i>1.56838</i>	<i>3.42773</i>	<i>1.56838</i>
HgO	-	-	-	-	-
KAlSiO <sub>4</sub>	-	-	-	-	-
La(OH) <sub>3</sub>	-	-	-	-	-
LaPO <sub>4</sub> •2H <sub>2</sub> O	<i>0.00010</i>	<i>0.00011</i>	<i>0.00005</i>	<i>0.00011</i>	<i>0.00005</i>
Mn(OH) <sub>2</sub>	-	-	-	-	-
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	<i>0.02970</i>	<i>0.03153</i>	<i>0.01443</i>	<i>0.03153</i>	<i>0.01443</i>
MnCO <sub>3</sub>	-	-	-	-	-
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	<i>0.47700</i>	<i>0.50633</i>	<i>0.23168</i>	<i>0.50633</i>	<i>0.23168</i>
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	<i>1.01941</i>	<i>1.08210</i>	<i>0.49512</i>	<i>1.08210</i>	<i>0.49512</i>
NaAlSiO <sub>4</sub>	<i>0.92570</i>	<i>0.98263</i>	<i>0.44961</i>	<i>0.98263</i>	<i>0.44961</i>
Ni(OH) <sub>2</sub>	<i>0.00496</i>	<i>0.00526</i>	<i>0.00241</i>	<i>0.00526</i>	<i>0.00241</i>
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-
NiC <sub>2</sub> O <sub>4</sub> •2H <sub>2</sub> O	-	-	-	-	-
Pb(OH) <sub>2</sub>	<i>0.01135</i>	<i>0.01205</i>	<i>0.00551</i>	<i>0.01205</i>	<i>0.00551</i>
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-
PbCO <sub>3</sub>	-	-	-	-	-
Pu(OH) <sub>4</sub>	<i>0.00004</i>	<i>0.00005</i>	<i>0.00002</i>	<i>0.00005</i>	<i>0.00002</i>
SiO <sub>2</sub>	-	-	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-
SrCO <sub>3</sub>	<i>0.04453</i>	<i>0.04727</i>	<i>0.02163</i>	<i>0.04727</i>	<i>0.02163</i>
TcO <sub>2</sub>	-	-	-	-	-
ZrO <sub>2</sub>	<i>0.00118</i>	<i>0.00125</i>	<i>0.00057</i>	<i>0.00125</i>	<i>0.00057</i>
KNO <sub>3</sub>	-	-	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	<i>0.04057</i>	-	-	-	-
Na <sub>2</sub> CO <sub>3</sub> •H <sub>2</sub> O	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub> •10H <sub>2</sub> O	-	-	-	-	-
Na <sub>3</sub> FSO <sub>4</sub>	-	-	-	-	-
Na <sub>3</sub> NO <sub>3</sub> SO <sub>4</sub> •H <sub>2</sub> O	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> •8H <sub>2</sub> O	-	-	-	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> •10H <sub>2</sub> O	<i>6.37408</i>	-	-	-	-
Na <sub>6</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-
NaF	<i>0.50793</i>	-	-	-	-
NaF(PO <sub>4</sub> ) <sub>2</sub> •19H <sub>2</sub> O	<i>0.66969</i>	-	-	-	-
NaHCO <sub>3</sub>	-	-	-	-	-
NaNO <sub>2</sub>	-	-	-	-	-
NaNO <sub>3</sub>	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> •0.25NaOH•12H <sub>2</sub> O	-	-	-	-	-
Total Volume % UDS	<i>14.63</i>	<i>7.47</i>	<i>3.42</i>	<i>7.47</i>	<i>3.42</i>
Solids Concentration (g/L)	<b>360.0</b>	<b>229.9</b>	<b>105.2</b>	<b>229.9</b>	<b>105.2</b>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

### Rheological Data

Model/model Parameter		<i>T-107</i>	<i>T-107</i>	<i>T-107</i>	<i>T-107</i>
Temperature (°C)		25	25	90	90
Source of Data					
Notes		Fit from hardcopies in Tingey archive file	Fit from hardcopies in Tingey archive file	Fit from hardcopies in Tingey archive file	Fit from hardcopies in Tingey archive file
<b>Newtonian:</b>					
$\eta$ – Newtonian viscosity (cP)		9.302	4.612	8.466	2.559
r – correlation coefficient		0.949	0.980	0.940	0.987
<b>Ostwald (or Power Law):</b>					
m – the consistency coefficient (Pa·s <sup>-n</sup> )		0.666	0.006	0.387	0.003
n – the power-law exponent		0.261	0.952	0.344	1.000
r – correlation coefficient		0.913	0.975	0.958	0.987
<b>Bingham Plastic:</b>					
$\tau_B$ – the Bingham yield stress (Pa)		0.852	0.049	0.630	0.000
$\eta_p$ – the plastic viscosity (Pa·s)		0.007	0.004	0.007	0.003
r – correlation coefficient		0.949	0.980	0.940	0.987
<b>Herschel-Bulkley:</b>					
$\tau_H$ – the yield stress (Pa)		0.735	0.050	0.415	0.000
k – the Herschel-Bulkely consistency coefficient (Pa·s <sup>-b</sup> )		0.039	0.004	0.088	0.003
b – the Herschel-Bulkely power-law exponent		0.710	1.000	0.574	1.000
r – correlation coefficient		0.965	0.980	0.971	0.987
n/a = not applicable					

### Physical Property Data

Physical Property	<i>T-107</i>	<i>T-107</i>	<i>T-107</i>	<i>T-107</i>	<i>T-107</i>
Notes					
Temperature (°C)	30	30	30	30	30
Zeta Potential (mV)					
Bulk Density (g/mL)	1.44	1.22	1.10	1.22	1.10
vol% Settled Solids	74	68	32	68	32
Density of Centrifuged Solids (g/mL)	1.53	1.44	1.32	1.44	1.32
vol% Centrifuged Solids	74	36	16	36	16
wt% Centrifuged Solids	79	44	19	44	19
Supernatant Density (g/mL)	1.20	1.07	1.03	1.07	1.03
Density of Settled Solids (g/mL)	n/m	n/m	n/m	n/m	n/m
wt% Settled Supernatant	n/m	n/m	n/m	n/m	n/m
wt% dissolved solids in supernatant	<i>23.17</i>	<i>20.66</i>	<i>19.89</i>	<i>20.66</i>	<i>19.89</i>
wt% total solids in Centrifuged Sludge	n/m	n/m	n/m	n/m	n/m
wt% Total Solids	47	n/m	n/m	n/m	n/m
wt% UDS	25.00	<i>18.84</i>	<i>9.56</i>	<i>18.84</i>	<i>9.56</i>
Density of Solids (g/cc)	<i>2.46</i>	<i>3.08</i>	<i>3.08</i>	<i>3.08</i>	<i>3.08</i>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Settling Data**

Settling Schedule		<i>T-107</i>	<i>T-107</i>		
Notes:		WHC-SD-WM-ER-382	WHC-SD-WM-ER-382		
Temperature (°C)		5-35	5-36		
Total initial volume		100	100		
5 minutes					
10 minutes					
15 minutes					
20 minutes					
30 minutes					
40 minutes					
50 minutes					
1 hour					
2 hours		95	65		
3 hours					
4 hours					
5 hours		89	56		
6 hours					
24 hours		72	41		
32 hours		70	36		
48 hours		68	32		
56 hours		67	32		
72 hours final settled					

**Shear Strength Data**

Shear Strength Schedule	<i>T-107</i>				
Source of Data	WHC-SD-WM-ER-382, rev 0				
Notes:	Page 6-7				
Temperature (°C)	Unspecified				
Description	Shear Vane at unspecified gel time or temperature				
Gelation Time/Shear Strength (Pa)					
5 minutes					
10 minutes					
15 minutes					
20 minutes					
30 minutes					
40 minutes					
50 minutes					
1 hour					
2 hours					
3 hours					
4 hours					
5 hours					
6 hours					
24 hours					
32 hours					
48 hours					
56 hours					
72 hours	720				
Infinte time (GRE)					

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

## Model Chemical Data From ESP

Analyte\Sample	T-110	T-110	T-110	T-110
Description	Tank Composite with water added to return to original solids content	30 wt% dilution of a core composite	1:1 Dilution of a core composite	4:1 Dilution of a core composite
Model Basis	Salty	Washed	Washed	Washed
Source of Data	PNNL-14365	PNNL-14365	PNNL-14365	PNNL-14365
Solid Phases (vol% of bulk)				
(NaAlO <sub>2</sub> ) <sub>2</sub> •2.5H <sub>2</sub> O	-	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	-	-	-	-
Bi <sub>2</sub> O <sub>3</sub>	<i>1.15553</i>	<i>0.63157</i>	<i>0.25860</i>	<i>0.05099</i>
BiOCl	-	-	-	-
Boehmite	-	-	-	-
Ca(OH) <sub>2</sub>	-	-	-	-
Ca <sub>3</sub> OH(PO <sub>3</sub> ) <sub>3</sub>	<i>0.00703</i>	<i>0.00384</i>	<i>0.00157</i>	<i>0.00031</i>
CaC <sub>2</sub> O <sub>4</sub> •H <sub>2</sub> O	-	-	-	-
CaCO <sub>3</sub>	-	-	-	-
CaF <sub>2</sub>	<i>0.32908</i>	<i>0.17986</i>	<i>0.07365</i>	<i>0.01452</i>
CrOOH	<i>0.17966</i>	<i>0.09820</i>	<i>0.04021</i>	<i>0.00793</i>
FeOOH	<i>2.54317</i>	<i>1.39000</i>	<i>0.56916</i>	<i>0.11221</i>
Gibbsite	-	-	-	-
HgO	-	-	-	-
KAlSiO <sub>4</sub>	-	-	-	-
La(OH) <sub>3</sub>	-	-	-	-
LaPO <sub>4</sub> •2H <sub>2</sub> O	<i>0.06452</i>	<i>0.03526</i>	<i>0.01444</i>	<i>0.00285</i>
Mn(OH) <sub>2</sub>	-	-	-	-
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	<i>0.19524</i>	<i>0.10671</i>	<i>0.04369</i>	<i>0.00861</i>
MnCO <sub>3</sub>	-	-	-	-
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	-	-	-	-
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	<i>1.77381</i>	<i>0.96950</i>	<i>0.39697</i>	<i>0.07827</i>
NaAlSiO <sub>4</sub>	<i>0.06315</i>	<i>0.03451</i>	<i>0.01413</i>	<i>0.00279</i>
Ni(OH) <sub>2</sub>	<i>0.01007</i>	<i>0.00551</i>	<i>0.00225</i>	<i>0.00044</i>
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-
NiC <sub>2</sub> O <sub>4</sub> •2H <sub>2</sub> O	-	-	-	-
Pb(OH) <sub>2</sub>	<i>0.05860</i>	<i>0.03203</i>	<i>0.01311</i>	<i>0.00259</i>
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-
PbCO <sub>3</sub>	-	-	-	-
Pu(OH) <sub>4</sub>	<i>0.00012</i>	<i>0.00006</i>	<i>0.00003</i>	<i>0.00001</i>
SiO <sub>2</sub>	-	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-
SrCO <sub>3</sub>	<i>0.05596</i>	<i>0.03059</i>	<i>0.01252</i>	<i>0.00247</i>
TcO <sub>2</sub>	<i>0.00000</i>	<i>0.00000</i>	<i>0.00000</i>	<i>0.00000</i>
ZrO <sub>2</sub>	<i>0.00076</i>	<i>0.00042</i>	<i>0.00017</i>	<i>0.00003</i>
KNO <sub>3</sub>	-	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	<i>0.14186</i>	-	-	-
Na <sub>2</sub> CO <sub>3</sub> •H <sub>2</sub> O	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub> •10H <sub>2</sub> O	-	-	-	-
Na <sub>3</sub> FSO <sub>4</sub>	-	-	-	-
Na <sub>3</sub> NO <sub>3</sub> SO <sub>4</sub> •H <sub>2</sub> O	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> •8H <sub>2</sub> O	-	-	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> •10H <sub>2</sub> O	<i>7.68168</i>	-	-	-
Na <sub>6</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-	-	-
NaF	-	-	-	-
NaF(PO <sub>4</sub> ) <sub>2</sub> •19H <sub>2</sub> O	-	-	-	-
NaHCO <sub>3</sub>	-	-	-	-
NaNO <sub>2</sub>	-	-	-	-
NaNO <sub>3</sub>	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> •0.25NaOH•12H <sub>2</sub> O	-	-	-	-
Total Volume % UDS	<i>14.26</i>	<i>3.52</i>	<i>1.44</i>	<i>0.28</i>
Solids Concentration (g/L)	<b>436.8</b>	<b>160.1</b>	<b>65.6</b>	<b>12.9</b>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

## Rheological Data

Model/model Parameter	T-110	T-110	T-110
Temperature (°C)	25	25	25
Source of Data	<i>PNNL-14365</i>	<i>PNNL-14365</i>	<i>PNNL-14365</i>
Instrumentation	Haake RS300 Concentric Cylinders with a 3 mm Gap	Haake RS300 Concentric Cylinders with a 3 mm Gap	Haake RS300 Concentric Cylinders with a 3 mm Gap
<b>Newtonian:</b>			
$\eta$ – Newtonian viscosity (cP)	n/a	n/a	1.41
r – correlation coefficient	n/a	n/a	0.94
<b>Ostwald (or Power Law):</b>			
m – the consistency coefficient (Pa·s <sup>-n</sup> )	n/a	n/a	n/a
n – the power-law exponent	n/a	n/a	n/a
r – correlation coefficient	n/a	n/a	n/a
<b>Bingham Plastic:</b>			
$\tau_B$ - the Bingham yield stress (Pa)	1.54	0.14	0.02
$\eta_p$ - the plastic viscosity (Pa·s)	0.0059	0.0023	0.0013
r – correlation coefficient	0.99	0.99	0.95
<b>Herschel-Bulkley:</b>			
$\tau_H$ - the yield stress (Pa)	1.11	0.07	n/a
k - the Herschel-Bulkely consistency coefficient (Pa·s <sup>-b</sup> )	0.02	0.01	n/a
b - the Herschel-Bulkely power-law exponent	0.82	0.83	n/a
r – correlation coefficient	0.99	0.99	n/a
n/a = not applicable			

## Physical Property Data

Physical Property	<i>T-110</i>	<i>T-110</i>	<i>T-110</i>	<i>T-110</i>
Source of Data	<i>PNNL-14365</i>	<i>PNNL-14365</i>	<i>PNNL-14365</i>	<i>PNNL-14365</i>
Temperature (°C)				
Zeta Potential (mV)				
Bulk Density (g/mL)	1.50	1.26	1.13	1.04
vol% Settled Solids	100	87.1	46.4	22.2
Density of Centrifuged Solids (g/mL)	1.58	1.51	1.61	1.47
vol% Centrifuged Solids	79.9	39.9	16.4	8.1
wt% Centrifuged Solids	<i>84</i>	<i>48</i>	<i>23</i>	<i>11</i>
Supernatant Density (g/mL)	1.24	1.14	1.08	1.03
Density of Settled Solids (g/mL)				
wt% Settled Supernatant				
wt% dissolved solids in supernatant				
wt% total solids in Centrifuged Sludge				
wt% Total Solids	48.4	29.3	15.3	6.4
wt% UDS	<i>29.12</i>	<i>12.71</i>	<i>5.80</i>	<i>1.24</i>
Density of Solids (g/cc)	<i>3.06</i>	<i>4.55</i>	<i>4.55</i>	<i>4.55</i>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.



**Settling Data**

Settling Schedule		PNNL-14365	PNNL-14365	PNNL-14365
Source of Data				
Temperature (°C)				
Total initial volume		13.7	13.6	13.5
5 minutes		13.7	13.6	13.3
10 minutes		13.7	13.6	12.5
15 minutes		13.7	13.4	11.9
20 minutes		13.7		
30 minutes		13.7	13.3	10.9
40 minutes		13.7		
50 minutes		13.7		
1 hour		13.7	12.2	5.9
2 hours		13.7	10.1	4.9
3 hours		13.7	8.9	4.4
4 hours		13.7	8.9	4.1
5 hours				
6 hours		13.45	8.45	3.15
24 hours				
32 hours		12.6	6.4	3
48 hours				3
56 hours				3
72 hours final settled		11.9	6.2	3

**Shear Strength Data**

Shear Strength Schedule	T-110			
Source of Data	PNNL-14365			
Instrumentation	Haake RS300 Shear Vane			
Temperature (°C)	25			
Description	Tank Composite with water added to return to original solids content (49%)			
Gelation Time/Shear Strength (Pa)				
5 minutes				
10 minutes				
15 minutes				
20 minutes				
30 minutes				
40 minutes				
50 minutes				
1 hour				
2 hours				
3 hours				
4 hours				
5 hours				
6 hours				
24 hours				
32 hours				
48 hours				
56 hours				
72 hours	70			
Infinte time (GRE)				

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

Model Chemical Data From ESP

Analyte/Sample	T-111	T-111	T-111	T-111	T-111	T-111	T-111	T-111	T-111
Description	Segment 2 Core 31	Segment 2 Core 31 1:1 Dilution	Segment 2 Core 31 1:1 Dilution	Segment 2 Core 31 3:1 Dilution	Segment 2 Core 31 3:1 Dilution	Segment 8 Core 31	Segment 8 Core 31 1:1 Dilution	Segment 8 Core 31 1:1 Dilution	Segment 8 Core 31 3:1 Dilution
Model Basis	Salty	Washed	Washed	Washed	Washed	Salty	Washed	Washed	Washed
Source of Data	SD-WM-DP-024	SD-WM-DP-024	SD-WM-DP-024	SD-WM-DP-024	SD-WM-DP-024	SD-WM-DP-024	SD-WM-DP-024	SD-WM-DP-024	SD-WM-DP-024
Solid Phases (vol% of bulk)									
(NaAlO <sub>2</sub> ) <sub>2</sub> ·2.5H <sub>2</sub> O	-	-	-	-	-	-	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	0.00385	0.00012	0.00012	0.00017	0.00017	0.00554	0.00192	0.00192	0.00071
Bi <sub>2</sub> O <sub>3</sub>	0.60186	0.01823	0.01823	0.02712	0.02712	0.86544	0.29978	0.29978	0.11028
BiOCl	-	-	-	-	-	-	-	-	-
Boehmite	-	-	-	-	-	-	-	-	-
Ca(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-
Ca <sub>2</sub> OH(PO <sub>4</sub> ) <sub>3</sub>	-	-	-	-	-	-	-	-	-
CuC <sub>2</sub> O <sub>4</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-
CaCO <sub>3</sub>	-	-	-	-	-	-	-	-	-
CaF <sub>2</sub>	0.22133	0.00671	0.00671	0.00997	0.00997	0.31826	0.11024	0.11024	0.04055
CrOOH	-	-	-	-	-	-	-	-	-
FeOOH	1.20472	0.03650	0.03650	0.05428	0.05428	1.73233	0.60006	0.60006	0.22074
Gibbsite	-	-	-	-	-	-	-	-	-
HgO	-	-	-	-	-	-	-	-	-
KAlSiO <sub>4</sub>	-	-	-	-	-	-	-	-	-
La(OH) <sub>3</sub>	-	-	-	-	-	-	-	-	-
LaPO <sub>4</sub> ·2H <sub>2</sub> O	0.22553	0.00683	0.00683	0.01016	0.01016	0.32430	0.11233	0.11233	0.04132
Mn(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	1.06760	0.03234	0.03234	0.04810	0.04810	1.53515	0.53176	0.53176	0.19561
MnCO <sub>3</sub>	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	-	-	-	-	-	-	-	-	-
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	0.15717	0.00476	0.00476	0.00708	0.00708	0.22600	0.07828	0.07828	0.02880
NaAlSiO <sub>4</sub>	-	-	-	-	-	-	-	-	-
Ni(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-
NiC <sub>2</sub> O <sub>4</sub> ·2H <sub>2</sub> O	0.03715	0.00113	0.00113	0.00167	0.00167	0.05341	0.01850	0.01850	0.00681
Pb(OH) <sub>2</sub>	-	-	-	-	-	-	-	-	-
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	0.00985	0.00030	0.00030	0.00044	0.00044	0.01416	0.00491	0.00491	0.00180
PbCO <sub>3</sub>	-	-	-	-	-	-	-	-	-
Pu(OH) <sub>4</sub>	0.00009	0.00000	0.00000	0.00000	0.00000	0.00013	0.00005	0.00005	0.00002
SiO <sub>2</sub>	0.24581	0.00745	0.00745	0.01108	0.01108	0.35347	0.12244	0.12244	0.04504
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-	-	-	-	-	-
SrCO <sub>3</sub>	0.02892	0.00088	0.00088	0.00130	0.00130	0.04159	0.01441	0.01441	0.00530
TcO <sub>2</sub>	-	-	-	-	-	-	-	-	-
ZrO <sub>2</sub>	0.00004	0.00000	0.00000	0.00000	0.00000	0.00006	0.00002	0.00002	0.00001
KNO <sub>3</sub>	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	0.41852	-	-	-	-	0.60182	-	-	-
Na <sub>2</sub> CO <sub>3</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-	-	-	-	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub> ·10H <sub>2</sub> O	-	-	-	-	-	-	-	-	-
Na <sub>7</sub> FSO <sub>4</sub>	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> NO <sub>3</sub> SO <sub>4</sub> ·H <sub>2</sub> O	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> ·8H <sub>2</sub> O	-	-	-	-	-	-	-	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> ·10H <sub>2</sub> O	2.39164	-	-	-	-	3.43905	-	-	-
Na <sub>6</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-	-	-	-	-	-	-	-
NaF	-	-	-	-	-	-	-	-	-
NaF(PO <sub>4</sub> ) <sub>2</sub> ·19H <sub>2</sub> O	-	-	-	-	-	-	-	-	-
NaHCO <sub>3</sub>	-	-	-	-	-	-	-	-	-
NaNO <sub>2</sub>	-	-	-	-	-	-	-	-	-
NaNO <sub>3</sub>	-	-	-	-	-	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> ·0.25NaOH·12H <sub>2</sub> O	-	-	-	-	-	-	-	-	-
Total Volume % UDS	6.61	0.12	0.12	0.17	0.17	9.51	1.89	1.89	0.70
Solids Concentration (g/L)	226.1	5.2	5.2	7.8	7.8	325.1	85.9	85.9	31.6

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Rheological Data**

Model/model Parameter									
Temperature (°C)		27	95	28	95		27	95	95
Source of Data	SD-WM-DP-024	SD-WM-DP-024	SD-WM-DP-024	SD-WM-DP-024	SD-WM-DP-024		SD-WM-DP-024	SD-WM-DP-024	SD-WM-DP-024
Instrumentation		Haake M500 MV1	Haake M500 MV1	Haake M500 MV1	Haake M500 MV1		Haake M500 MV1	Haake M500 MV1	Haake M500 MV1
<b>Newtonian:</b>									
$\eta$ - Newtonian viscosity (cP)		n/a	n/a	1.76	1.60		n/a	n/a	n/a
r - correlation coefficient		n/a	n/a				n/a	n/a	n/a
<b>Ostwald (or Power Law):</b>									
m - the consistency coefficient (Pa·s <sup>-n</sup> )		n/a	n/a	n/a	n/a		n/a	n/a	n/a
n - the power-law exponent		n/a	n/a	n/a	n/a		n/a	n/a	n/a
r - correlation coefficient		n/a	n/a	n/a	n/a		n/a	n/a	n/a
<b>Bingham Plastic:</b>									
$\tau_B$ - the Bingham yield stress (Pa)		1.05	1.04	0.27	0.24		0.58	0.79	0.25
$\eta_p$ - the plastic viscosity (Pa·s)		0.0038	0.0008	0.0018	0.0016		0.0054	0.0026	0.0016
r - correlation coefficient		1.00	0.73	0.99	0.97		0.99	0.98	0.96
<b>Herschel-Bulkley:</b>									
$\tau_H$ - the yield stress (Pa)		n/a	n/a	n/a	n/a		0.36	n/a	n/a
k - the Herschel-Bulkely consistency coefficient (Pa·s <sup>-b</sup> )		n/a	n/a	n/a	n/a		0.0258	n/a	n/a
b - the Hershel-Bulkely power-law exponent		n/a	n/a	n/a	n/a		0.75	n/a	n/a
r - correlation coefficient		n/a	n/a	n/a	n/a		1.00	n/a	n/a
n/a = not applicable									

**Physical Property Data**

Physical Property	T-111	T-111	T-111	T-111	T-111	T-111	T-111	T-111	T-111
Source of Data	SD-WM-DP-024	SD-WM-DP-024	SD-WM-DP-024	SD-WM-DP-024	SD-WM-DP-024	SD-WM-DP-024	SD-WM-DP-024	SD-WM-DP-024	SD-WM-DP-024
Temperature (°C)									28
Zeta Potential (mV)									
Bulk Density (g/mL)	1.19	<i>1.06</i>	<i>1.06</i>	<i>1.03</i>	<i>1.03</i>	1.28	<i>1.12</i>	<i>1.12</i>	<i>1.05</i>
vol% Settled Solids	100	85.7		52.1		100	78.1		36.4
Density of Centrifuged Solids (g/mL)	1.22					1.22			
vol% Centrifuged Solids	65.8					71.9			
wt% Centrifuged Solids	67					76			
Supernatant Density (g/mL)	1.07	<i>1.06</i>	<i>1.06</i>	<i>1.03</i>	<i>1.03</i>	1.1	<i>1.06</i>	<i>1.06</i>	<i>1.03</i>
Density of Settled Solids (g/mL)									
wt% Settled Supernatant	0					0			
wt% dissolved solids in supernatant									
wt% total solids in Centrifuged Sludge									
wt% Total Solids	22.4					29.3			
wt% UDS	19.00	<i>0.49</i>	<i>0.49</i>	<i>0.75</i>	<i>0.75</i>	25.40	<i>7.67</i>	<i>7.67</i>	<i>3.01</i>
Density of Solids (g/cc)	<i>3.42</i>	<i>4.54</i>	<i>4.54</i>	<i>4.54</i>	<i>4.54</i>	<i>3.42</i>	<i>4.54</i>	<i>4.54</i>	<i>4.54</i>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Settling Data**

Settling Schedule		T-111		T-111		T-111	
Source of Data		SD-WM-DP-024		SD-WM-DP-024		SD-WM-DP-024	
Temperature (°C)		29		28		29	
Total initial volume		11		11.9		11.8	
5 minutes							
10 minutes							
15 minutes		11		11.8		11.8	
20 minutes							
30 minutes		11		11.6		11.8	
40 minutes							
50 minutes							
1 hour		10.7		11.2		11.6	
2 hours		10.6		10.8		11.5	
3 hours		10.5		10.2		11.5	
4 hours		10.4		9.6		11.5	
5 hours		10.3		8.9		11.4	
6 hours		10.2		8.5		11.3	
24 hours		9.5		6.3		10.3	
32 hours		9.4		6.2		10.2	
48 hours		9.3		6.2		9.6	
56 hours		9.3		6.2		9.2	
72 hours final settled		9.3		6.2		9.2	

**Shear Strength Data**

Shear Strength Schedule	T-111					T-111		
Source of Data	SD-WM-DP-024 Personal Communication with JM Tingey					SD-WM-DP-024 Personal Communication with JM Tingey		
Instrumentation	Haake M500 Shear Vane					Haake M500 Shear Vane		
Temperature (°C)	30					30		
Description	Segment 2 Core 31					Segment 8 Core 31		
Gelation Time/Shear Strength (Pa)								
5 minutes								
10 minutes								
15 minutes								
20 minutes								
30 minutes								
40 minutes								
50 minutes								
1 hour								
2 hours								
3 hours								
4 hours								
5 hours								
6 hours								
24 hours								
32 hours								
48 hours								
56 hours								
72 hours								
Infinte time (GRE)	180					450		

## Model Chemical Data From ESP

Analyte\Sample	T-203	T-203	T-203	T-203
Description	Homogenized Tank Composite	30 wt% dilution of a core composite	1:1 Dilution of a core composite	4:1 Dilution of a core composite
Model Basis	Salty	Washed	Washed	Washed
Source of Data	PNNL-14365	PNNL-14365	PNNL-14365	PNNL-14365
Solid Phases (vol% of bulk)				
(NaAlO <sub>2</sub> ) <sub>2</sub> •2.5H <sub>2</sub> O	-	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	<i>0.00003</i>	<i>0.00010</i>	<i>0.00004</i>	<i>0.00001</i>
Bi <sub>2</sub> O <sub>3</sub>	<i>0.33825</i>	<i>1.00803</i>	<i>0.39795</i>	<i>0.13122</i>
BiOCl	-	-	-	-
Boehmite	-	-	-	-
Ca(OH) <sub>2</sub>	-	-	-	-
Ca <sub>2</sub> OH(PO <sub>4</sub> ) <sub>3</sub>	-	-	-	-
CaC <sub>2</sub> O <sub>4</sub> •H <sub>2</sub> O	-	-	-	-
CaCO <sub>3</sub>	-	-	-	-
CaF <sub>2</sub>	<i>0.01498</i>	<i>0.04465</i>	<i>0.01763</i>	<i>0.00581</i>
CrOOH	-	-	-	-
FeOOH	<i>0.10698</i>	<i>0.31881</i>	<i>0.12586</i>	<i>0.04150</i>
Gibbsite	-	-	-	-
HgO	-	-	-	-
KAlSiO <sub>4</sub>	<i>0.00888</i>	<i>0.02645</i>	<i>0.01044</i>	<i>0.00344</i>
La(OH) <sub>3</sub>	-	-	-	-
LaPO <sub>4</sub> •2H <sub>2</sub> O	<i>0.20946</i>	<i>0.62422</i>	<i>0.24643</i>	<i>0.08126</i>
Mn(OH) <sub>2</sub>	<i>0.26426</i>	<i>0.78753</i>	<i>0.31090</i>	<i>0.10252</i>
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-
MnCO <sub>3</sub>	<i>0.14380</i>	<i>0.42855</i>	<i>0.16918</i>	<i>0.05579</i>
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	<i>0.00152</i>	<i>0.00452</i>	<i>0.00178</i>	<i>0.00059</i>
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	-	-	-	-
NaAlSiO <sub>4</sub>	-	-	-	-
Ni(OH) <sub>2</sub>	<i>0.00402</i>	<i>0.01197</i>	<i>0.00473</i>	<i>0.00156</i>
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-
NiC <sub>2</sub> O <sub>4</sub> •2H <sub>2</sub> O	-	-	-	-
Pb(OH) <sub>2</sub>	<i>0.00022</i>	<i>0.00067</i>	<i>0.00026</i>	<i>0.00009</i>
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-
PbCO <sub>3</sub>	-	-	-	-
Pu(OH) <sub>4</sub>	<i>0.00004</i>	<i>0.00013</i>	<i>0.00005</i>	<i>0.00002</i>
SiO <sub>2</sub>	-	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-
SrCO <sub>3</sub>	<i>0.01695</i>	<i>0.05051</i>	<i>0.01994</i>	<i>0.00657</i>
TcO <sub>2</sub>	-	-	-	-
ZrO <sub>2</sub>	<i>0.00003</i>	<i>0.00009</i>	<i>0.00004</i>	<i>0.00001</i>
KNO <sub>3</sub>	-	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	-	-	-	-
Na <sub>2</sub> CO <sub>3</sub> •H <sub>2</sub> O	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub> •10H <sub>2</sub> O	-	-	-	-
Na <sub>3</sub> FSO <sub>4</sub>	-	-	-	-
Na <sub>3</sub> NO <sub>3</sub> SO <sub>4</sub> •H <sub>2</sub> O	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> •8H <sub>2</sub> O	-	-	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> •10H <sub>2</sub> O	-	-	-	-
Na <sub>6</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-	-	-
NaF	-	-	-	-
NaF(PO <sub>4</sub> ) <sub>2</sub> •19H <sub>2</sub> O	-	-	-	-
NaHCO <sub>3</sub>	-	-	-	-
NaNO <sub>2</sub>	-	-	-	-
NaNO <sub>3</sub>	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> •0.25NaOH•12H <sub>2</sub> O	-	-	-	-
Total Volume % UDS	<i>1.11</i>	<i>3.31</i>	<i>1.31</i>	<i>0.43</i>
Solids Concentration (g/L)	<b>63.0</b>	<b>187.7</b>	<b>74.1</b>	<b>24.4</b>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

## Rheological Data

Model/model Parameter	T-203	T-203	T-203
Temperature (°C)	25	25	25
Source of Data	PNNL-14365	PNNL-14365	PNNL-14365
Instrumentation	Haake RS300 Concentric Cylinders with a 3 mm Gap	Haake RS300 Concentric Cylinders with a 3 mm Gap	Haake RS300 Concentric Cylinders with a 3 mm Gap
<b>Newtonian:</b>			
$\eta$ – Newtonian viscosity (cP)	n/a	n/a	n/a
r – correlation coefficient	n/a	n/a	n/a
<b>Ostwald (or Power Law):</b>			
m – the consistency coefficient (Pa·s <sup>-n</sup> )	n/a	n/a	n/a
n – the power-law exponent	n/a	n/a	n/a
r – correlation coefficient	n/a	n/a	n/a
<b>Bingham Plastic:</b>			
$\tau_B$ - the Bingham yield stress (Pa)	35.50	3.18	0.10
$\eta_p$ - the plastic viscosity (Pa·s)	0.0148	0.0031	0.0015
r – correlation coefficient	0.99	1.00	1.00
<b>Herschel-Bulkley:</b>			
$\tau_H$ - the yield stress (Pa)	n/a	n/a	n/a
k - the Herschel-Bulkely consistency coefficient (Pa·s <sup>-b</sup> )	n/a	n/a	n/a
b - the Herschel-Bulkely power-law exponent	n/a	n/a	n/a
r – correlation coefficient	n/a	n/a	n/a
n/a = not applicable			

## Physical Property Data

Physical Property	T-203	T-203	T-203	T-203
Source of Data	PNNL-14365	PNNL-14365	PNNL-14365	PNNL-14365
Temperature (°C)				
Zeta Potential (mV)				
Bulk Density (g/mL)	1.22	1.29	1.14	1.05
vol% Settled Solids	100	100	92.8	44.8
Density of Centrifuged Solids (g/mL)	1.39	1.3	1.31	1.29
vol% Centrifuged Solids	87.6	71.5	38.6	15.0
wt% Centrifuged Solids	<i>100</i>	<i>72</i>	<i>44</i>	<i>18</i>
Supernatant Density (g/mL)	1.17	1.14	1.08	1.03
Density of Settled Solids (g/mL)				
wt% Settled Supernatant				
wt% dissolved solids in supernatant				
wt% total solids in Centrifuged Sludge				
wt% Total Solids	34.3	30.7	16.4	6.4
wt% UDS	<i>5.16</i>	<i>14.55</i>	<i>6.50</i>	2.33
Density of Solids (g/cc)	<i>5.68</i>	<i>5.68</i>	<i>5.68</i>	<i>5.68</i>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Settling Data**

Settling Schedule			PNNL-14365	PNNL-14365
Source of Data				
Temperature (°C)				
Total initial volume			13.7	13.4
5 minutes			13.7	
10 minutes			13.7	13.1
15 minutes			13.7	12.7
20 minutes			13.7	12.2
30 minutes			13.7	11.7
40 minutes			13.7	
50 minutes			13.7	
1 hour			13.7	10.1
2 hours			13.7	7.9
3 hours			13.5	7.2
4 hours			13.4	7
5 hours				
6 hours				
24 hours			13	6.3
32 hours				6.3
48 hours			12.7	6.3
56 hours			12.7	6.2
72 hours final settled			12.7	6.2

**Shear Strength Data**

Shear Strength Schedule	T-203	T-203		
Source of Data	PNNL-14365	PNNL-14365		
Instrumentation	Haake RS300 Shear Vane	Haake RS300 Shear Vane		
Temperature (°C)	25	25		
Description	Homogenized Tank Composite	30 wt% dilution of the tank composite		
Gelation Time/Shear Strength (Pa)				
5 minutes				
10 minutes				
15 minutes				
20 minutes				
30 minutes				
40 minutes				
50 minutes				
1 hour				
2 hours				
3 hours				
4 hours				
5 hours				
6 hours				
24 hours				
32 hours				
48 hours				
56 hours				
72 hours	3770	310		
Infinte time (GRE)				

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

## Model Chemical Data From ESP

Analyte\Sample	T-204	T-204	T-204	T-204
Description	Homogenized Tank Composite	30 wt% dilution of a core composite	1:1 Dilution of a core composite	4:1 Dilution of a core composite
Model Basis	Salty	Washed	Washed	Washed
Source of Data	PNNL-14365	PNNL-14365	PNNL-14365	PNNL-14365
Solid Phases (vol% of bulk)				
(NaAlO <sub>2</sub> ) <sub>2</sub> •2.5H <sub>2</sub> O	-	-	-	-
Ag <sub>2</sub> CO <sub>3</sub>	<i>0.00002</i>	<i>0.00011</i>	<i>0.00005</i>	<i>0.00001</i>
Bi <sub>2</sub> O <sub>3</sub>	<i>0.21416</i>	<i>1.13735</i>	<i>0.49136</i>	<i>0.13952</i>
BiOCl	-	-	-	-
Boehmite	-	-	-	-
Ca(OH) <sub>2</sub>	-	-	-	-
Ca <sub>2</sub> OH(PO <sub>4</sub> ) <sub>3</sub>	-	-	-	-
CaC <sub>2</sub> O <sub>4</sub> •H <sub>2</sub> O	-	-	-	-
CaCO <sub>3</sub>	-	-	-	-
CaF <sub>2</sub>	<i>0.00419</i>	<i>0.02226</i>	<i>0.00962</i>	<i>0.00273</i>
CrOOH	<i>0.00512</i>	<i>0.02717</i>	<i>0.01174</i>	<i>0.00333</i>
FeOOH	<i>0.05008</i>	<i>0.26599</i>	<i>0.11491</i>	<i>0.03263</i>
Gibbsite	-	-	-	-
HgO	-	-	-	-
KAlSiO <sub>4</sub>	<i>0.00340</i>	<i>0.01806</i>	<i>0.00780</i>	<i>0.00222</i>
La(OH) <sub>3</sub>	-	-	-	-
LaPO <sub>4</sub> •2H <sub>2</sub> O	<i>0.11411</i>	<i>0.60603</i>	<i>0.26182</i>	<i>0.07434</i>
Mn(OH) <sub>2</sub>	<i>0.23176</i>	<i>1.23083</i>	<i>0.53175</i>	<i>0.15098</i>
Mn <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-
MnCO <sub>3</sub>	-	-	-	-
Na <sub>2</sub> U <sub>2</sub> O <sub>7</sub>	<i>0.00112</i>	<i>0.00593</i>	<i>0.00256</i>	<i>0.00073</i>
NaAlCO <sub>3</sub> (OH) <sub>2</sub>	-	-	-	-
NaAlSiO <sub>4</sub>	-	-	-	-
Ni(OH) <sub>2</sub>	<i>0.00309</i>	<i>0.01641</i>	<i>0.00709</i>	<i>0.00201</i>
Ni <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-
NiC <sub>2</sub> O <sub>4</sub> •2H <sub>2</sub> O	-	-	-	-
Pb(OH) <sub>2</sub>	<i>0.00158</i>	<i>0.00838</i>	<i>0.00362</i>	<i>0.00103</i>
Pb <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-
PbCO <sub>3</sub>	-	-	-	-
Pu(OH) <sub>4</sub>	<i>0.00001</i>	<i>0.00008</i>	<i>0.00003</i>	<i>0.00001</i>
SiO <sub>2</sub>	-	-	-	-
Sr <sub>3</sub> (PO <sub>4</sub> ) <sub>2</sub>	-	-	-	-
SrCO <sub>3</sub>	<i>0.00797</i>	<i>0.04230</i>	<i>0.01828</i>	<i>0.00519</i>
TcO <sub>2</sub>	-	-	-	-
ZrO <sub>2</sub>	<i>0.00001</i>	<i>0.00004</i>	<i>0.00002</i>	<i>0.00000</i>
KNO <sub>3</sub>	-	-	-	-
Na <sub>2</sub> C <sub>2</sub> O <sub>4</sub>	-	-	-	-
Na <sub>2</sub> CO <sub>3</sub> •H <sub>2</sub> O	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub>	-	-	-	-
Na <sub>2</sub> SO <sub>4</sub> •10H <sub>2</sub> O	-	-	-	-
Na <sub>3</sub> FSO <sub>4</sub>	-	-	-	-
Na <sub>3</sub> NO <sub>3</sub> SO <sub>4</sub> •H <sub>2</sub> O	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> •8H <sub>2</sub> O	-	-	-	-
Na <sub>4</sub> P <sub>2</sub> O <sub>7</sub> •10H <sub>2</sub> O	-	-	-	-
Na <sub>6</sub> (SO <sub>4</sub> ) <sub>2</sub> CO <sub>3</sub>	-	-	-	-
NaF	-	-	-	-
NaF(PO <sub>4</sub> ) <sub>2</sub> •19H <sub>2</sub> O	-	-	-	-
NaHCO <sub>3</sub>	-	-	-	-
NaNO <sub>2</sub>	-	-	-	-
NaNO <sub>3</sub>	-	-	-	-
Na <sub>3</sub> PO <sub>4</sub> •0.25NaOH•12H <sub>2</sub> O	-	-	-	-
Total Volume % UDS	<i>0.64</i>	<i>3.38</i>	<i>1.46</i>	<i>0.41</i>
Solids Concentration (g/L)	<b>37.3</b>	<b>197.9</b>	<b>85.5</b>	<b>24.3</b>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.



**Rheological Data**

Model/model Parameter			T-204	T-204
Temperature (°C)			25	25
Source of Data			<i>PNNL-14365</i>	<i>PNNL-14365</i>
Instrumentation			Haake RS300 Concentric Cylinders with a 3 mm Gap	Haake RS300 Concentric Cylinders with a 3 mm Gap
<b>Newtonian:</b>				
$\eta$ – Newtonian viscosity (cP)			n/a	n/a
r – correlation coefficient			n/a	n/a
<b>Ostwald (or Power Law):</b>				
m – the consistency coefficient (Pa·s <sup>-n</sup> )			n/a	n/a
n – the power-law exponent			n/a	n/a
r – correlation coefficient			n/a	n/a
<b>Bingham Plastic:</b>				
$\tau_B$ - the Bingham yield stress (Pa)			3.11	0.19
$\eta_p$ - the plastic viscosity (Pa·s)			0.0038	0.0019
r – correlation coefficient			1.00	1.00
<b>Herschel-Bulkley:</b>				
$\tau_H$ - the yield stress (Pa)			n/a	0.14
k - the Herschel-Bulkely consistency coefficient (Pa·s <sup>-b</sup> )			n/a	0.0052
b - the Herschel-Bulkely power-law exponent			n/a	0.83
r – correlation coefficient			n/a	1.00
n/a = not applicable				

**Physical Property Data**

Physical Property	T-204	T-204	T-204	T-204
Source of Data	<i>PNNL-14365</i>	<i>PNNL-14365</i>	<i>PNNL-14365</i>	<i>PNNL-14365</i>
Temperature (°C)				
Zeta Potential (mV)				
Bulk Density (g/mL)	1.17	1.28	1.13	1.05
vol% Settled Solids	100	100	88	46.2
Density of Centrifuged Solids (g/mL)	1.4	1.36	1.3	1.35
vol% Centrifuged Solids	83.7	79.9	40	16.7
wt% Centrifuged Solids	<i>100</i>	<i>85</i>	<i>46</i>	<i>21</i>
Supernatant Density (g/mL)	1.14	1.12	1.06	1.03
Density of Settled Solids (g/mL)				
wt% Settled Supernatant				
wt% dissolved solids in supernatant				
wt% total solids in Centrifuged Sludge				
wt% Total Solids	31.5	29.4	14.6	6.1
wt% UDS	<i>3.18</i>	<i>15.46</i>	<i>7.56</i>	<i>2.31</i>
Density of Solids (g/cc)	<i>5.85</i>	<i>5.85</i>	<i>5.85</i>	<i>5.85</i>

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

### Settling Data

Settling Schedule			PNNL-14365	PNNL-14365
Source of Data				
Temperature (°C)				
Total initial volume			13.6	13.1
5 minutes			13.6	12.8
10 minutes			13.6	11.6
15 minutes			13.6	10.6
20 minutes			13.6	10.1
30 minutes			13.6	9
40 minutes			13.6	
50 minutes			13.6	
1 hour			13.6	7.6
2 hours			13.45	7.2
3 hours			13.4	6.8
4 hours			13.2	6.6
5 hours				
6 hours			13.1	6.6
24 hours			12.5	6.6
32 hours				
48 hours			12	6.5
56 hours			12	6.5
72 hours final settled			12	6.5

### Shear Strength Data

Shear Strength Schedule	<i>T-204</i>	<i>T-204</i>	<i>T-204</i>	
Source of Data	PNNL-14365	PNNL-14365	PNNL-14365	
Instrumentation	Haake RS300 Shear Vane	Haake RS300 Shear Vane	Haake RS300 Shear Vane	
Temperature (°C)	25	25	25	
Description	Homogenized Tank Composite	30 wt% dilution of the tank composite	Settled Solids from the 1:1 Dilution (18.0 wt% total solids)	
Gelation Time/Shear Strength (Pa)				
5 minutes				
10 minutes				
15 minutes				
20 minutes				
30 minutes				
40 minutes				
50 minutes				
1 hour				
2 hours				
3 hours				
4 hours				
5 hours				
6 hours				
24 hours				
32 hours				
48 hours				
56 hours				
72 hours	1520	842	20	
Infinte time (GRE)				

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.



**Physical Property Data**

Physical Property	U-103	U-103	U-103	U-103	U-103	U-103	U-103	U-103	U-103	U-103	U-103	U-103	U-103	U-103	U-103	U-103	U-103	U-103
Source of Data																		
Temperature (°C)																		
Zeta Potential (mV)																		
Bulk Density (g/mL)	1.61	1.76	1.70	1.72	1.76	1.70	1.68	1.68	1.80	1.80	1.90	1.45	1.80	1.80	1.80	1.74	1.45	1.78
vol% Settled Solids																		
Density of Centrifuged Solids (g/mL)																		
vol% Centrifuged Solids																		
wt% Centrifuged Solids																		
Supernatant Density (g/mL)	1.45	1.45	1.45	1.45	1.45	1.45	1.45	1.45	1.45	1.45	1.45	1.45	1.45	1.45	1.45	1.45	1.45	1.45
Density of Settled Solids (g/mL)																		
wt% Settled Supernatant																		
wt% dissolved solids in supernatant																		
wt% total solids in Centrifuged Sludge																		
wt% Total Solids																		
wt% UDS	29.27	51.27	42.94	45.78	51.27	42.94	40.03	40.03	56.52	56.52	68.67	0.79	56.52	56.52	56.52	48.56	0.79	53.93
Density of Solids (g/cc)	2.22	2.22	2.22	2.22	2.22	2.22	2.22	2.22	2.22	2.22	2.22	2.22	2.22	2.22	2.22	2.22	2.22	2.22

**Shear Strength Data**

Shear Strength Schedule	U-103	U-103	U-103	U-103	U-103	U-103	U-103	U-103	U-103	U-103	U-103	U-103	U-103	U-103	U-103	U-103	U-103	U-103
Source of Data	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249
Instrumentation	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer
Temperature (°C)	26	26	29	29	29	29	29	29	28	28	28	26	26	29	29	29	26	26
Description	Riser 13 Depth from bottom of tank is 160 inches	Riser 13 Depth from bottom of tank is 140 inches	Riser 13 Depth from bottom of tank is 110 inches	Riser 13 Depth from bottom of tank is 100 inches	Riser 13 Depth from bottom of tank is 85 inches	Riser 13 Depth from bottom of tank is 70 inches	Riser 13 Depth from bottom of tank is 60 inches	Riser 13 Depth from bottom of tank is 50 inches	Riser 13 Depth from bottom of tank is 25 inches	Riser 13 Depth from bottom of tank is 18 inches	Riser 13 Depth from bottom of tank is 10 inches	Riser 7 Depth from bottom of tank is 170 inches	Riser 7 Depth from bottom of tank is 135 inches	Riser 7 Depth from bottom of tank is 120 inches	Riser 7 Depth from bottom of tank is 110 inches	Riser 7 Depth from bottom of tank is 78 inches	Riser 2 Depth from bottom of tank is 167 inches	Riser 2 Depth from bottom of tank is 157 inches
Gelation Time/Shear Strength (Pa)																		
5 minutes																		
10 minutes																		
15 minutes																		
20 minutes																		
30 minutes																		
40 minutes																		
50 minutes																		
1 hour																		
2 hours																		
3 hours																		
4 hours																		
5 hours																		
6 hours																		
24 hours																		
32 hours																		
48 hours																		
56 hours																		
72 hours																		
Infinte time (GRE)	100	200	1750	1300	500	1200	800	20	700	150	1000	50	70	150	200	1000	60	250



**Physical Property Data**

Physical Property	<i>U-107</i>	<i>U-107</i>	<i>U-107</i>	<i>U-107</i>	<i>U-107</i>	<i>U-107</i>	<i>U-107</i>	<i>U-107</i>	<i>U-107</i>	<i>U-107</i>	<i>U-107</i>	<i>U-107</i>
Source of Data												
Temperature (°C)												
Zeta Potential (mV)												
Bulk Density (g/mL)	1.76	1.76	1.76	1.76	1.76	1.76	1.76	1.78	1.78	1.78	1.74	1.78
vol% Settled Solids												
Density of Centrifuged Solids (g/mL)												
vol% Centrifuged Solids												
wt% Centrifuged Solids												
Supernatant Density (g/mL)	1.47	1.47	1.47	1.47	1.47	1.47	1.47	1.47	1.47	1.47	1.47	1.47
Density of Settled Solids (g/mL)												
wt% Settled Supernatant												
wt% dissolved solids in supernatant												
wt% total solids in Centrifuged Sludge												
wt% Total Solids												
wt% UDS	55.78	55.78	55.78	55.78	55.78	55.78	55.78	58.93	58.93	58.93	52.54	58.93
Density of Solids (g/cc)	2.09	2.09	2.09	2.09	2.09	2.09	2.09	2.09	2.09	2.09	2.09	2.09

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

**Shear Strength Data**

Shear Strength Schedule	U-107	U-107	U-107	U-107	U-107	U-107	U-107	U-107	U-107	U-107	U-107	U-107
Source of Data	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249
Instrumentation	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer
Temperature (°C)	25	25	25	25	25	25	25	25	25	25	25	25
Description	Riser 9 Depth from bottom of tank is 137 inches	Riser 9 Depth from bottom of tank is 128 inches	Riser 9 Depth from bottom of tank is 118 inches	Riser 9 Depth from bottom of tank is 112 inches	Riser 9 Depth from bottom of tank is 108 inches	Riser 7 Depth from bottom of tank is 131 inches	Riser 7 Depth from bottom of tank is 112 inches	Riser 7 Depth from bottom of tank is 102 inches	Riser 7 Depth from bottom of tank is 93 inches	Riser 7 Depth from bottom of tank is 82 inches	Riser 7 Depth from bottom of tank is 79 inches	Riser 7 Depth from bottom of tank is 73 inches
Gelation Time/Shear Strength (Pa)												
5 minutes												
10 minutes												
15 minutes												
20 minutes												
30 minutes												
40 minutes												
50 minutes												
1 hour												
2 hours												
3 hours												
4 hours												
5 hours												
6 hours												
24 hours												
32 hours												
48 hours												
56 hours												
72 hours												
Infinte time (GRE)	15	20	25	50	70	50	150	50	200	550	130	380

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.





**Physical Property Data**

Physical Property	<i>U-107</i>	<i>U-107</i>	<i>U-107</i>	<i>U-107</i>	<i>U-107</i>	<i>U-107</i>	<i>U-107</i>	<i>U-107</i>	<i>U-107</i>	<i>U-107</i>	<i>U-107</i>	<i>U-107</i>
Source of Data												
Temperature (°C)												
Zeta Potential (mV)												
Bulk Density (g/mL)	1.64	1.72	1.72	1.75	1.75	1.67	1.85	1.69	1.75	1.82	1.77	1.77
vol% Settled Solids												
Density of Centrifuged Solids (g/mL)												
vol% Centrifuged Solids												
wt% Centrifuged Solids												
Supernatant Density (g/mL)	1.47	1.47	1.47	1.47	1.47	1.47	1.47	1.47	1.47	1.47	1.47	1.47
Density of Settled Solids (g/mL)												
wt% Settled Supernatant												
wt% dissolved solids in supernatant												
wt% total solids in Centrifuged Sludge												
wt% Total Solids												
wt% UDS	35.21	49.24	49.24	54.17	54.17	40.63	69.45	44.13	54.17	65.04	57.36	57.36
Density of Solids (g/cc)	2.09	2.09	2.09	2.09	2.09	2.09	2.09	2.09	2.09	2.09	2.09	2.09

**Shear Strength Data**

Shear Strength Schedule	U-107	U-107	U-107	U-107	U-107	U-107	U-107	U-107	U-107	U-107	U-107	U-107
Source of Data	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249	RPP-7249
Instrumentation	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer	Ball Rheometer
Temperature (°C)	25	25	25	23	25	25	25	25	25	25	25	25
Description	Riser 7 Depth from bottom of tank is 70 inches	Riser 7 Depth from bottom of tank is 58 inches	Riser 7 Depth from bottom of tank is 54 inches	Riser 2 Depth from bottom of tank is 141 inches	Riser 2 Depth from bottom of tank is 137 inches	Riser 2 Depth from bottom of tank is 77 inches	Riser 2 Depth from bottom of tank is 62 inches	Riser 2 Depth from bottom of tank is 58 inches	Riser 2 Depth from bottom of tank is 55 inches	Riser 2 Depth from bottom of tank is 50 inches	Riser 2 Depth from bottom of tank is 40 inches	Riser 2 Depth from bottom of tank is 12 inches
Gelation Time/Shear Strength (Pa)												
5 minutes												
10 minutes												
15 minutes												
20 minutes												
30 minutes												
40 minutes												
50 minutes												
1 hour												
2 hours												
3 hours												
4 hours												
5 hours												
6 hours												
24 hours												
32 hours												
48 hours												
56 hours												
72 hours												
Infinte time (GRE)	380	50	400	30	50	375	300	450	230	100	225	50

Note: Numbers in italics are calculated values. Numbers in normal font are reported data.

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