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Fracture Enhanced Soil Vapor Extraction Technology Demonstration at the A-014 Outfall

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The methods presented in this document may be patented or patent pending through the United States Patent Office.

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BACKGROUND

M-Area process wastewaters were discharged from buildings in the M-Area to the A-014 Outfall from 1952 through 1980. It is estimated that 1.5 million pounds of chlorinated solvents may have been released to the A-014 Outfall through the sewer line. The majority of the solvents released was tetrachloroethylene (PCE) and to a lesser degree trichloroethylene (TCE). Small amounts of 1,1,1-trichloroethane (TCA) were also released.

Groundwater monitoring well data from the early 1980s indicated a cVOC (chlorinated volatile organic compound) source zone in the area of the present water discharge at the A-014 Outfall. The central sector groundwater recovery system includes well RWM-6, located adjacent to the outfall. Characterization work in the vadose zone was initiated in the early 1990s and a soil vapor extraction (SVE) remediation unit was put on-line in 1995.

The characterization work performed to date has shown that the majority of the vadose zone cVOC contamination associated with the outfall is located between 10 and 35 feet below the ground surface (Riha and Rossabi 2003). The solvent contamination is located in low permeability, fine-grained sediments that are difficult to remediate with traditional SVE, which is dependent upon moving large quantities of air through the vadose zone and the contaminated media.

Previous SVE testing in M-Area indicates that the shallow sediments have low air permeability. These sediments have historically produced flow rates less than 10 scfm when tested with a traditional SVE system. Therefore, hydraulic fracturing was proposed to improve the permeability of these types of sediments, making them more suitable for treatment with traditional SVE. This fine grained zone is known as the Upland Unit and is fairly consistent in physical properties across the Savannah River Site A/M Areas.

The South Carolina Department of Health and Environmental Control (SCDHEC) granted the Savannah River Site (SRS) a Temporary Authorization (TA) to conduct a technology demonstration of fracture enhanced SVE at the A-014 Outfall (Haynes 2006). Fracture enhanced SVE is being used to remediate the shallow low permeability sediment contaminated with DNAPL (dense non-aqueous phase liquid) consisting cVOCs at the A-014 Outfall. The Savannah River National Laboratory (SRNL) is performing the testing and evaluation of fracture enhanced SVE.

Polychlorinated biphenyls (PCBs) were present on the filter media from the SVE unit near the A-014 Outfall; and there is the possibility that PCBs are present in the area. Therefore, in December 2006 the SRS submitted a request for a modification to the riskbased Toxic Substances Control Act (TSCA) approval for the M-Area Settling Basin (MASB) Dynamic Underground Stripping (DUS) Project to allow the processing of the A-014 purge water through the MASB DUS Remediation System (Flora 2006). The MASB DUS Project contains a PCB treatment (filtering) system, referred to as the Mycelx Filter Skid. In May 2007, the U. S. Environmental Protection Agency provided approval to allow co-disposal of the contaminated purge water from the A-014 SVE process with the DUS effluent for treatment and disposal (Banister 2007).

PROJECT DESCRIPTION

The Savannah River Site (SRS) installed eight hydraulic fractured wells to enhance SVE for the treatment of solvent contamination in the Upland Unit at the A-014 Outfall at the Savannah River Site. A pilot study proving the value of SVE enhanced with soil fracturing was conducted in M-Area in FY05. Introducing propant-filled fractures into these tight zones improves the performance of SVE by 1) increasing the overall permeability of the formation and thereby increasing SVE flow rates, 2) shortening diffusion pathways, and 3) increasing air permeability by improving pore water removal. The synergistic effect of the fracture well completion methods, fracture and flow geometry, and pore water removal appears to increase the rate of solvent mass removal over that of increasing flow rate alone (Riha, Dixon et al. 2005).

PCE DNAPL is still present at the A-014 Outfall after years of SVE, which has only effectively treated the more permeable zones below the Upland Unit. This DNAPL zone is located directly beneath the original outfall infrastructure. The volume of soil containing DNAPL is approximately 50,800 ft³ (1900 yd³). The DNAPL zone is approximately 20 ft thick with a maximum depth of 35 ft. To reduce the long-term threat of this source area, SVE enhanced with soil hydraulic fracturing was initiated for the Upland Unit at the A-014 Outfall.

FRACTURING RESULTS

The fracture wells were constructed of 3.25 inch diameter Geoprobe push rods (fracture casing) with an annulus large enough for 2 inch schedule 40 PVC pipe. The fracture wells were installed in September 2006 by direct push techniques and the fracturing was completed in January 2007. Injections were done with the approval of Underground Injection Control Permit #874.

The hydraulic fractures were created in a manner similar to that outlined in the document "Hydraulic Fracturing Technology, Technology Evaluation Report" (USEPA, 1993). Following this method, a radial notch was cut into the vadose zone sediments at the end of the fracture casing using a high pressure jetting tool referred to as a lance. This notch was used to initiate a hydraulic fracture. At the A-14 Outfall, the notches were made in a half circle towards the middle of the original outfall in an attempt to guide the fractures towards the source area (see Figure 1).

After the sediments were notched, a slurry of cross-linked guar gum gel and sand was injected at a constant flow rate into the 2-inch well using a progressive cavity pump. Injection was accomplished using a specialized mixer and pump operated by the subcontractor FRx, Inc. The purpose of the guar gum was to create a gel capable of suspending high concentrations of sand. An enzyme was added to the slurry to break

down the gel several hours after injection. Once injection ceases, the resulting fracture starts to close as the gel seeps into the formation. The fracture is then held open by the sand (propant) that is left behind.

The injection pressure measured at the well-head increased abruptly to approximately 125 psi at the start of injection and then decreased as the fracture started to propagate. Pressure fluctuated during the first few minutes as the sand content in the gel was increased from small values up to the target load for the fracture. The pressure was typically in the range of 50 psi to 100 psi when the full load of sand in the slurry was being injected. Table 1 provides a summary of the results of the fracture injections. Five of the eight fractures were considered successful. Failures are attributed to the multitude of abandoned boreholes at the site from previous characterization and testing.

Well	Fracture	Fracture	Sand,	
ID	Depth, ft	Date	lbs	Comments
				Vented to surface quickly at several
				locations. This Fracture well could
AF-1	18	1/8/2007	0	not be salvaged.
AF-2	26	1/4/2007	2800	Fracture installed as planned.
				Vented to surface quickly at several
				locations. This Fracture well could
AF-3	11	1/3/2007	0	not be salvaged.
				Bridged 2 times in either the hose or
				well. Cleaned out and continued
AF-4	23	1/4/2007	2000	injection. Fracture successful.
AF-5	18	1/4/2007	1800	Fracture installed as planned.
				Vented around annulus. Tried to add
				grout to seal annulus. Retry on
AF-6	11	1/4/2007	0	1/8/07 was unsuccessful
				Vented to surface at the very end of
				injection. Fracture considered
AF-7	17	1/8/2007	2000	successful
AF-8	23	1/4/2007	2800	Fracture installed as planned.

Table 1 – Summary of Fracture Injections

SVE WELL SETUP

The five viable fractures were equipped for vapor extraction by flushing the remaining sand from the fracture casing and placing 2 inch diameter schedule 40 PVC pipe wells inside the casing. The wells had 10 slot 5 ft screens with a bottom cap. Shrink tubing and a bead of vacuum grease were used to seal the steel casing and PVC well together. The seals were tested by placing a high vacuum on the well and checking for leaks with cigar smoke.

The hydraulic fracture wells were completed with an atmospheric air inlet valve at the wellhead. Using a tee at the top of the wellhead, tubing was inserted down to the bottom of the wells and connected to the inlets. During long term testing the valves were controlled by solenoid valves that would open periodically to let atmospheric air flow in through the valve, down the tubing, and into the bottom of the well casing. This was done to increase air-flow velocity within the well casing to remove standing water that may accumulate during SVE operation.

The wells were connected to a manifold using cam-lock fittings and 2 inch flexible hose. A liquid ring vapor extraction unit equipped with a large capacity (2,000 gal) moisture knock-out tank was used to remove water and contaminants from the fractured sediments.

Additionally, two vertical arrays of monitoring points were installed to monitor the performance of the system. Each array consists of a Flexible Liner Underground Technology (FLUTe) liner equipped with six monitoring ports at 5 ft intervals ranging from 10 to 35 ft deep. Figure 1 provides the locations of the fracture wells and monitoring arrays.



Figure 1 - Plan View of the Well Locations

FRACTURE WELL PERFORMANCE – FLOW RATES

The fracture wells were evaluated to determine flow characteristics and zone of influence. Flow measurements were made on each fracture well at three different pressures to evaluate the well flow performance. These tests were conducted on two different dates to evaluate any changes in the flow performance of the wells over time. The tests were conducted by running the SVE system at 5, 10, and 15 in Hg vacuum for 15 minutes each on each fracture well. The results of the two tests are presented graphically in Figure 2 and Figure 3. Note that well MVE-13 is also included in Figure 2. MVE-13 is a conventionally installed vertical well screened from 17-27 ft and the data is used for comparison with the performance of the fracture wells. The flow rate for MVE-13 at 15 in Hg was 6.2 scfm.

Two sets of wells (AF-2, 4, 5 and AF-7, 8) were run continuously at maximum vacuum between these two flow tests. The flow rates decreased significantly for the majority of the wells except for AF-2 (Table 2).

Detailed discussions are provided on these field tests and some longer-term tests in Appendix A. The reason for the decrease in flow rate is a decrease in permeability. The reasons theorized for the decrease in permeability are primarily related to water infiltration and are listed below.

- 1. Increase in water saturation (decrease in relative permeability) due to increased rainfall between the two testing events.
- 2. Clogging of the fracture sand with fine grain materials due to liquefaction during high water saturations and high vacuums. Particularly fractures AF-5 and AF-7 that are located in the shallower fine-grained material.

	Flow Ra	te at 15 in				
	Hg,	scfm				
Fracture						
Well ID	6/5/2007	7/19/2007	Flow Rate			
AF-2	28.7	27.5	4%			
AF-4	17.3	9.5	45%			
AF-5	38.0	3.2	92%			
AF-7	4.1	1.4	66%			
AF-8	79.2	52.2	34%			

Table 2 – Decrease in Fracture Well Flow Rates



Figure 2 – Fracture Well Flow versus Pressure on 6/5/07



Figure 3 – Fracture Well Flow versus Pressure on 7/19/07

FRACTURE WELL PERFORMANCE – ZONE OF INFLUENCE

The zone of influence (ZOI) is defined here as a differential pressure between the extraction location (fracture) and other areas in the subsurface that would create air flow and mass removal. One can visualize a fracture SVE well as a horizontal disk or pancake in the subsurface with air-flow moving vertically (upwards and downwards) towards the fracture. Air-flow also occurs laterally towards the fracture due to the pressure gradients. Vertical cVOC removal was envisioned for the DNAPL source at the A-014 Outfall using the fractures, therefore, pressures were measured at 5 ft depth intervals at two locations (AFLT-1 and 2). See location map in Figure 1 for fracture well and monitoring point locations.

Figure 4 provides subsurface vacuum pressure response from the four fracture wells that provided adequate flow for remediation (AF-2, 4, 5 and 8). The plots show the subsurface pressure at the two monitoring locations after 45 minutes of flow. The wells were tested individually at 15 in Hg vacuum. This data was collected during the 6/5/07 flow testing and provides a snapshot of the ZOI at that time but should provide a relative representation of the ZOI for each fracture. This data was used to illustrate the ZOI because the other SVE unit (3M) in the area was not operating. The 3M SVE unit would skew the vacuums in the deeper monitoring points since it is treating the sandy unit below the Upland Unit. The shaded region shows the depth of the fracture initiation. The fracture may dip upward or downward from the initiation point depending on the geology and previous borings nearby. The distance from the pressure monitoring points and fracture well (initiation point) is also shown on the plots.

Overall, each of the fractures show influence both vertically and laterally for moving air, water, and cVOCs towards the fractures for removal. The increasing vacuums with depth are due to the permeability increase with depth in the Upland Unit. The geologic setting is upper coastal plain where the Upland Unit was created in a fining upward depositional setting.

Fracture wells AF-2, 4 and 5 show the greatest influence for the vertical removal of the cVOCs in the source zone. The pressure gradients show the cVOCs will move both upward and downward towards the fractures for removal. These fractures are also closest to the main DNAPL source area. The ZOI will increase as the system is run constantly and under higher vacuum pressures.

The fracture wells show a significant lateral influence (up to 80 ft). No pressure response was seen in the monitoring points when testing the conventional vertical well (MVE-13) in the same formation and location (data not shown).

The mass transfer in the Upland Unit will be faster below the fractures and slower above the fractures due the permeability differences. Overall, the viable fracture SVE wells provide adequate coverage of the DNAPL source area for remediation.



Figure 4 – Subsurface Vacuum Response during Flow Testing of Individual Fracture Wells

CONCENTRATION TRENDS AND MASS REMOVAL

The SVE unit operated nearly continuously from 6/19/07 to 12/2/07 with several short down periods for maintenance. See operational history in Appendix B. The SVE system failed on 12/2/07 due to a failure of the drive shaft between the pump and motor that required the purchase and installation of a new pump and motor (the test unit was 12 years old at the time).

Tetrachloroethylene (PCE), trichloroethylene (TCE), and carbon dioxide (CO₂) concentration data were measured with an infrared photo-acoustic spectrometer (IRPAS). Additional gas chromatography (GC) analysis was also completed for air emission reporting. The IRPAS data corresponds well with the GC data. All analytical data is provided in Appendix C with a comparison of the IRPAS and GC data.

The operational data is provided graphically in Figure 5. The plot shows the flow and vacuum measurements, the start time for the different well configurations, the PCE concentration, and mass removal rates. Decreases in flow rate along with increases in vacuum are related to water movement towards the fractures and the resulting decrease in air permeability.



Figure 5 – Graphical Operational Data

Figure 6 shows the PCE concentration, flow rate, and rainfall from 8/10/07 to 12/2/07 for fracture wells AF-2 and AF-4 to illustrate the influence of rainfall on the ZOI due to reduced relative permeability. A significant decrease in concentration is evident after rainfall events indicating a reduced ZOI in the contaminated area. The heart of the contaminated area is beneath the outfall that carries storm water runoff. The decrease in concentration is more likely a shift in the ZOI as air is removed from portions of the fractures that are not directly beneath the outfall. These portions of the fractures would receive less infiltration. However, the concentrations and ZOI rebound after a period of time following the rainfall events. The time it takes for the infiltrating water to influence the ZOI appears to be on the order of one week. The overall influence is related to the frequency of rainfall events. The rainfall from the middle of August to the middle of September decreased the PCE concentration rebounded over the next month to 900 ppmv during low rainfall but decreased again during the next significant rainfall events. Overall, the flow rate was not affected significantly by rainfall for these two wells.



Figure 6 - Flow Rate, PCE Concentration and Rainfall for AF-2 and AF-4

Mass removal was calculated from the concentration and flow data. The mass removed form 6/19/07 to 12/2/07 was 2,507 lbs PCE and 46.7 lbs TCE, and the cumulative mass removed over time is shown in Figure 7. During this time period, the mass removal rate has changed with the rainfall events but rebounds after the ZOI recovers during dryer periods. The overall concentration and mass removal did not decline during this testing period, suggesting that the system removed the cVOCs from the source (DNAPL) area. Once this DNAPL source area becomes depleted, an exponentially declining concentration trend is expected.



WATER AND DNAPL REMOVAL

Water removal from the fracture wells was not measured directly because rainwater from the containment for the knockout tank was placed in the tank for disposal. The rainfall total in the area for the operating period was 21 inches and the containment was 12 ft x 12 ft. This results in approximately 1,900 gallons in the tank from rainfall. The tank contained approximately 2,000 gallons when emptied so approximately 100 gallons of pore water was removed from the fracture wells (ignoring evaporation of standing rainwater, which could be significant). Water removal from the fractures was expected to be greater, the reason for the low water removal from the fractures is unknown. DNAPL also was not observed in the tank.

It can be theorized that pore water moving into the fracture is draining downward prior to removal through the wells. This hypothesis is based on the observation of flow changes with rainfall (water is migrating towards the fractures) and the possibility of the fractures intercepting more conductive pathways for downward water migration. Several of the wells were observed to be sucking air due to the influence of SVE Unit 3M, indicating pathways to the sandy unit below the Upland Unit. This scenario is not necessarily detrimental since a soil vapor extraction well is operating in the sandy unit below the fracture zone to intercept any contaminants migrating downward with the water.

SUMMARY AND CONCLUSIONS

Data collected during this study show that the performance of hydraulically fractured wells (with respect to mass removal rates) may tend to decrease with time following precipitation events. These effects are due to temporary increases in water saturation in the formation within the vicinity of the fractures, therefore, the wells should tend to rebound during subsequent dry periods. The data available for fractured well versus conventional well performance (with respect to flow rate versus vacuum pressure) are limited in this study. However, the data that we have to draw from suggest that, with the possible exception of a few extreme examples, hydraulically fractured wells tend to perform better than conventional wells during SVE operation at the A-14 Outfall.

The pancake like geometry associated with hydraulic fractures also leads to a significant increase in ZOI, as compared to conventional wells. The increase in ZOI is due to the radially extending, horizontal, high-permeability conduit nature of the hydraulic fracture, however, air-flow into the fracture is predominately vertical (occurring at right angles to the fracture plane). Flow rates from above and below the fracture will tend to be equivalent when the formation is homogeneous, however, in the case of directionally fining depositional sequences flow rates will be greater from the direction of increasing permeability. The Upland Unit is a fining upward sequence, therefore flow rates (and contaminant mass flow rates) will tend to be higher below the fracture. This suggests that emplacing the fractures slightly above the source zone is an important strategy for accelerating contaminant removal at the A-014 Outfall site and in the Upland Unit at the SRS. However, due to the multitude of previous borings at the A-014 Outfall site, the shallower fractures failed.

More than 2500 lbs of cVOCs were removed during approximately 6 months of fractured well SVE operation at the A-014 field site. Plotting total mass removed over this time period shows a roughly linear relationship Figure 7. This occurs because the mass removal rate remains fairly constant with time. When mass removal comes predominately from cVOCs stored in the vapor phase there is a marked decline in mass removal rate over a short period of time due to the limiting nature of diffusion. Constant mass removal rates suggest that a source zone has been directly targeted and, therefore, is providing a constant supply of cVOC that partitions into the vapor phase and is removed through the well. Directly targeting and removing source zones is the most efficient approach to remediating contaminated sites.

Results of this study show that utilization of hydraulic fractures during SVE is an effective approach for increasing remediation efficiency at the A-014 Outfall field site and in the Upland Unit at the SRS. Hydraulically fractured wells tend to produce greater flow rates and create larger ZOI's than do conventional wells. These attributes allow fractured wells to effectively treat larger volumes of formation. The unique sand-emplacement geometry associated with hydraulically fractured wells also allows direct targeting of multiple zones located at similar elevations within a fairly large radius of the well. The ability to directly target source zones significantly decreases diffusion pathways, therefore, significantly decreasing the time required to reach remediation goals.

RECOMMENDATIONS

The following recommendations are based on the data collected to date:

- 1. Continue operation of a high vacuum SVE unit on the fracture wells that are targeting the source area (AF-2, 4 and possibly 5) until mass removal rates begin to decline indicating source depletion. After source depletion, connect well AF-8. Although at a lower concentration, it should produce 5-8 lbs per day for a short period of time due to its high flow rate.
- 2. Perform periodic well performance testing to determine any degradation or improvement of the fracture wells and periodic ZOI testing to verify source area treatment coverage. The recommend frequency is semi-annually
- 3. Once the source zone depletion is indicated, evaluate more passive remediation techniques such as enhanced attenuation (EA) methods for finally polishing (i.e. edible oils and enhanced biodegradation)

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Appendix A - Field Tests to Evaluate the A-14 Outfall SVE Fracture Wells

Richard Hall (SCUREF, Ph. D. Candidate, Clemson University)

Field tests were designed to characterize the performance of hydraulically fractured SVE wells located in the A-14 outfall area at SRS. Tests were conducted on five hydraulic fracture wells (AF-2,4,5,7,8) and a conventional well located in the test area that is part of a pre-existing SVE system (MVE-13) (Figure 1). Of the hydraulic fracture wells AF-5 and AF-7 were completed at relatively shallow depths (18 and 17 ft. respectively), whereas AF-2, 4, and 8 were deeper (26, 23, and 23 ft respectively). Well MVE-13 is screened from 17 to 27 below ground surface. Multi-level monitoring wells were also installed (AFLT-1 and AFLT-2) with pressure ports located at depths of 10, 15, 20, 25, 30, and 35 ft (Figure 1).

The hydraulic fracture wells were completed with an atmospheric air inlet valve at the well head. Tubing was inserted down to the bottom of the wells and connected to the inlets. During long term testing the valves were controlled by solenoid valves that would open periodically to let atmospheric air flow in through the valve, down the tubing, and into the bottom of the well casing. This was done to increase air flow velocity within the well casing to remove standing water that may accumulate during SVE operation.



Figure 1- Locations of wells tested at A-14 field site.

Pressure step tests were designed to investigate the relationship between flow rate out of the well and applied vacuum. The subsurface pressure distribution induced around the wells during tests was also of interest, as this data could potentially provide information about formation properties and/or radius of influence. The pre-existing SVE system (3M) located at the field site was turned off at least 24 hours prior to the initiation of individual well tests to prevent pressure influences from other wells. Before any sequence of tests was initiated pressure readings were taken from the monitoring wells. If the pressure values measured were not equal to zero then the pressure readings obtained during testing were adjusted by that amount. This was done to ensure that the subsurface pressures analyzed resulted from stress induced by vacuum application and not from barometric pressure fluctuations.

The pressure step tests were conducted by applying constant vacuum over a period of 15 minutes while monitoring air mass-flow rate out of the well. Near the end of the 15-minute period pressure measurements were taken at each of the ports in the monitoring wells and in the surrounding fracture wells. The vacuum pressure was then increased and the process repeated. The tests were typically done using 3 vacuum pressures (5, 10, and 15 in Hg). After a test was completed the system was allowed to re-equilibrate for half an hour before starting a test on another well.

Well Test Results

Well testing involved three phases. The first phase was conducted on 6-11-07 and consisted of a pressure step test on each of the wells. The second phase was conducted from 6-19-07 to 7-16-07. Phase 2 involved longer-term tests on selected wells that were manifold together while applying the maximum vacuum that the SVE unit was capable of producing. The third phase was conducted on 7-17-07 and consisted of repeating the pressure step test on each of the wells.

Phase 1 Tests

Results from the first pressure step tests conducted on 6-11-07 show that well AF-8 performed better than any of the other wells by at least a factor or 2 (~80 scfm @ 15 in Hg vacuum), followed by wells AF-5 (~38 scfm @ 15 in Hg vacuum), AF-2 (~29 scfm @ 15 in Hg vacuum), and AF-4 (~18 scfm @ 15 in Hg vacuum); with the conventional well (MVE-13) performing poorly as compared to the fractured wells (~7 scfm @ 15 in Hg vacuum) (Figure 2). Well AF-7 showed anomalous behavior in that the flow rate actually decreased after increases in vacuum pressure (Figure 2). During the lowest vacuum portion of the test well AF-7 behaved similarly to well AF-4, but produced the lowest flow rate observed for any of the wells (including the conventional well) under 15 in Hg (~4 scfm). There do not seem to be any trends associated with flow rate verses either well completion depth, or volume of sand used to create the fractures.

With the exception of well AF-7, the way that flow rate increases with increasing vacuum pressure is similar for the fractured wells. Flow rate increases are greater for steps at lower pressures than for steps at higher pressures (Figure 2), suggesting that the flow rate increase with pressure may be asymptotic. However, the flow rate with pressure behavior for the conventional well differs in that flow rate increases approximately linearly (Figure 2). Similar differences in flow rate verses pressure relationships for fractured and conventional wells have been observed in previous work, and are thought to be the consequence of differences in air-flow geometry (Hall, 2005).



Figure 2- Results from pressure step tests conducted on 6-05-07.

Phase 2 Tests

Long term well tests conducted from 6-19-07 to 6-22 and from 6-28-07 to 7-09-07 involved manifolding wells AF-2, 4, and 5. Wells AF-7 and 8 were manifolded for testing from 7-09-07 to 7-16-6-07. No testing was conducted from 6-22-07 to 6-28-28 due to equipment malfunction. Flow rate verses pressure data presented for phase 2 tests have been manually smoothed to remove spikes produced during gas sampling events. Dates on the x-axis correspond to the start of each day (midnight, 00:00)

During the longer-term tests the vacuum applied was the maximum that the SVE unit was capable of producing (air bypass valve on SVE unit was completely closed). Therefore when there was lesser resistance to flow (greater formation permeability, greater relative permeability, or the extreme case where the inlet is open to the atmosphere) then the vacuum pressure will be small and the air-flow rate will be large. However, when there is greater resistance to flow (lower formation permeability, lower relative permeability, or the extreme case where the inlet is plugged) then the vacuum pressure will be large and the air-flow rate will be small. Under these conditions there is a standard relationship between vacuum pressure and flow rate that is a function of the constant power produced by the SVE unit.

Tests conducted from 6-19-07 to 6-22-07 did not use solenoid valves on the atmospheric inlet valve; the valve was opened manually during sampling events to remove water from the well casings prior to sampling. Results from this test (Figure 3a) show that there was a fairly rapid decrease in flow rate (accompanied by the corresponding increase in vacuum pressure) during approximately the first hour of the test (flow started at 72 scfm but not shown to accentuate other data). The flow rate then shows an increase as a result of activities associated with a sampling event 1 (opening atmospheric valves to remove water) that took place at 14:30 on 6-19-07. After sampling event 1 the flow rate again decreased for approximately 5 hours then stayed fairly

constant for approximately 14 hours. The flow rate then increases during sampling event 2 that occurring around 10:30 on 6-20-07 and, following a short term decrease, the flow rate remained fairly constant for a period of approximately 5 hours. Sampling event 3 occurred at 16:40 on 6-20-07 and marked the start of a rapid decrease in flow rate (31% decrease) over a period of approximately 6 hours. The flow rate then begins to rebound again, however, subsequently decreases after sampling events 4 and 5 at 9:30 and 13:45 on 6-21-07. The test was then disrupted due to equipment malfunction.



Figure 3- Results from Phase 2 tests with Wells AF-2, 4, and 5 manifolded. a) 6-19 to 6-22 and b) from 6-28 to 7-09 (Sampling events are numbered in circles)

The AF-2, 4, 5 test was restarted on 6-28-07 with the solenoid valves installed and set to open every 45 minutes (Figure 3b). The flow rate at the start of the test was greater than flow rate at the end of the previous test (54 scfm as opposed to s43 cfm), which is to be expected because the system had time to re-equilibrate (re-pressurize). The flow rate, however, was significantly less than the initial flow rate of the first test (54 scfm as opposed to 72 scfm), which suggests some type of change in the system.

From 6-28-07 to 7-03-07 the flow rate decreases (Figure 3b). As seen during the first test (Figure 3a), abrupt decreases in flow rate seem to correlate with sampling events. The only exception is a sampling event that occurred at 14:30 on 6-29-07 where flow increased for a short time afterwards. The flow rate decreases to a point and becomes fairly constant starting around 7-3-07. At this point the responses of flow rate to sampling events stopped occurring. There is, however, a small magnitude cyclic pattern in the data that continues until the end of the test (more visible in pressure data). This is probably either due to solenoid valve dewatering activity or, more likely, due to fluctuations in barometric pressure.

Beginning on 7-9-07, a long-term test on wells AF- 7 and 8 was conducted. The flow rate with time data shows that sampling events caused the increase followed by decrease in flow rate pattern observed during the previous long-term tests on wells AF 2, 4, and 5. However, the flow rate data shows a fairly smooth, nearly linear decrease over the 7 day period if these sampling "blips" are ignored (accompanied by the corresponding nearly linear increase in vacuum pressure) (Figure 4). This pattern is most visible during the 7-14-07 to 7-16-17 portion of the test over which samples were not taken (Figure 4).



Figure 4- Results from Phase 2 tests with Wells AF-7 and 8 manifolded. (Sampling events are numbered in circles)

Phase 3 Tests

Results from the second round of pressure step tests conducted on 7-19-07 show that well AF- 8 again performed better than any of the other wells by nearly a factor of 2 (~52 scfm @ 15 in Hg vacuum), followed by wells AF-2 (~28 scfm @ 15 in Hg vacuum), and AF-4 (~10 scfm @ 15 in Hg vacuum), and AF-5 (~3 scfm @ 15 in Hg vacuum) (Figure 5). Well AF-7 again showed anomalous behavior in that the flow rate decreased as higher vacuum pressures were applied, and was again the worst performer of the fractured wells (Figure 2). Phase 3 test data for well MVE-13 is unavailable due to a problem during testing (well shutoff valve was closed).



Figure 5- Results from pressure step tests conducted on 7-19-07. (Notice difference in y-axis for figures 2 and 5).

The well performance rankings from Phase 1 and Phase 2 are similar, with the exception of well AF-5. AF-5 was the second best performing well during the 6-11-07 pressure step tests, however, the ranking decreased to second from last during the 7-19-07 tests. While Well AF-5 was an extreme case, the flow rates at various vacuum pressures decreased for all of the wells (Figure 6). Well AF-2 showed the smallest decrease in flow rate (4%); the AF-2 result plots from the different tests are actually very similar (Figure 6). Wells AF-4, 7, and 8 showed intermediate decreases in flow rate (45%, 66%, and 34% respectively). Well AF-5 was the extreme case with a 92% reduction in flow rate (Figure 6).



Figure 6- Comparison of 6-11-07 and 7-19-07 test results for all wells. (Notice AF-8 plot y-axis is different from others)

Discussion

When a vacuum is applied to an SVE well the flow rate will start out high and then decrease with time to some equilibrium mass flow rate. The pressure within the formation around the well screen is roughly atmospheric prior to the start of vacuum pumping. When pumping is initiated the pressure within the formation around the well screen decreases as air flows into and out of the well. Much of the air produced during early vacuum pumping is removed from formation storage in this way. As pumping continues the pressure front created by the SVE well migrates greater distances away from the well screen (radius of influence increases with time). The rate at which subsurface pressure changes decreases with time as air mass from atmospheric influences (or other open wells) becomes the primary source of air flow to the well. This continues until an equilibrium radius of influence/vacuum pressure condition is reached (Figure 7). This equilibrium is reached when the air mass supplied from the surrounding subsurface and atmosphere becomes equal to the air mass produced from the well.

Abrupt fluctuations in flow rate and vacuum pressure observed during phase 2 testing can mostly be attributed to sampling events. Prior to sampling, each of the manifolded wells was isolated under maximum vacuum and the atmospheric air inlet valve was opened to remove water from the well casing. Opening the atmospheric inlet valve causes a large increasing spike in flow rate along with a large decreasing spike in vacuum pressure (these are the spikes that were removed during the data smoothing process). The act of opening the wells to the atmosphere also has the effect of increasing the pressure (decreasing the vacuum) to some degree within the formation around the well screen. The partial re-pressurization along with the fact that water may have been removed from the well casing accounts for the increase in flow rate associated with some sampling events (evident in sampling events 1, 2, 3, 4, 16, 18, and 19 (Figures 3 and 4)).



Figure 7- Results of constant vacuum simulation showing tendency of flow rate to decrease with time during SVE operation.

The sampling and dewatering processes typically cause an increase in flow rate, however, it is expected that the flow rate should decrease over a fairly short period of time following the sampling event as the system goes back to equilibrium. Theoretically it should return back too, or near too the pre-sampling flow rate and then continue following whatever trend was present (typically decreasing or constant). However, according to phase 2 field test data this was not always the case. Following the post sample re-equilibration period for the AF-2, 4, 5 tests the flow rates were significantly decreased for sampling events 1, 3, 5, 6, and 8 (as compared to the pre-sampling flow rates) (Figure 3a,b). In contrast, flow rates were increased after the re-equilibration period for sampling events 2, 4, and 7 (Figure 3a,b). Sampling events 9 through 14 occurred during a period when the system seems to have reached an equilibrium condition, and did not significantly effect flow rate one way or the other (Figure 3b).

Results from the AF-7, 8 phase 2 test were more representative of what would be expected theoretically (Figure 4). There is a general decrease in flow rate during the test that is to be expected to some extent as the system goes to equilibrium. However, there may be another process responsible for some of the decrease as it is roughly linear in the field test data, whereas, decrease to equilibrium under constant conditions is a negative exponential (Figure 7). In any case, the data trend and flow rate were reasonably resumed following the disruptions induced by sampling events (Sample events 18 and 19 are good examples) (Figure 4).

During the phase 2 tests the tendency was for flow rate to decrease either gradually (Figure 4) or abruptly (Figure 3, following sampling event 3). As described before a negative exponential (gradual) decrease is expected early, however, this property of expected flow transience does not seem to account for all of the flow reduction observed during phase 2 tests. This becomes evident when considering the fact that the flow rates observed during the 7-19-07 pressure step tests were consistently less than those observed during the 6-11-07 tests (Figure 6). In each case the system (subsurface) was not stressed in any way at least 24 hours prior to testing. Obtaining consistently differing results from the two sets of tests suggests that some systematic change in the system occurred during the period of time between the tests. The most pressing questions put forth by these results are: What caused the systematic decrease in well performance for the fractured wells? and What caused the particularly extreme decrease in well performance of well AF-5 and the anomalous behavior of well AF-7?

The most plausible explanation for decrease in flow rate would be a decrease in permeability (or relative permeability) of the formation or the material filling the hydraulic fractures. A decrease in relative permeability would occur due to an increase in formation water saturation. This is a distinct possibility considering that during the 2 month period leading up to the first round of tests there was relatively little rain fall, however, the period just before and during the testing phase were comparatively rainy (Figure 8). A particularly heavy 3-day rain event occurred a week prior to the initial tests, and it also rained the day before the initial tests (Figure 8). The infiltration rates at the test site are probably fairly slow, considering the moderate to low permeability of the upper 4 to 5 ft of the upland unit. The formation material located at depths near the hydraulic fractures may have been relatively dry due to lack of rainfall during the previous 2 months, which would facilitate high flow rates during the first round of tests. By the time that the second round of tests were conducted the infiltrating water may have

had adequate time to reach the fracture depths and decrease relative permeability, and thus decrease flow rates during the second round of tests. The phase 2, long-term tests were conducted between the two rounds of pressure step tests. Application of high vacuum to the wells over this period would have expedited the infiltration of water near the surface to the depths around the hydraulic fractures.



Figure 8- Record of precipitation leading up too, and during well testing period.

Decreasing the relative permeability of the formation within the radius of influence of an SVE well will decrease the mass flow rate. However, applying a vacuum to a well (particularly the extreme vacuums applied during phase 2 testing) will cause pore water to flow towards the well screen and into the casing. If the water is systematically removed from the casing, using solenoid valves on atmospheric valves for instance, then the majority of the water in the formation near the well would be removed in a fairly short period of time. This scenario was investigated using a simple modeling approach. The model involved running an SVE well at constant pressure until an acceptably equilibrated state was reached. At this point the water saturation in the cells within the vicinity of the well screen was increased to 0.3. This caused an abrupt decrease in flow rate (Figure 9). The flow rate, however, rebounded to near the presaturation value fairly quickly (within 2 days) as the water was pulled toward the well screen and removed from the system (Figure 9). The time that it would take for this process to occur would depend on properties of the formation (this simulation was not calibrated to field conditions in any way), however, if infiltration of water is responsible for decreasing flow rate then the system should rebound eventually. Further evaluation of later field pumping data may be required to conclude whether this will/has happened or not.



Figure 9- Results from infiltration simulation.

Another explanation for decreases in flow rates may be some change effected on the physical properties (other than saturation alone) of the formation material and/or fracture material. An explanation such as this seems particularly required for the extreme case observed in well AF-5 and the anomalous behavior of well AF-7. A possible scenario that would account for this change is if there was some liquefaction of formation materials during SVE testing. This would not be unlikely given the increased water saturation and abrupt pressure change conditions associated with the rain events and abrupt starts/stops of vacuum on the wells during sampling. If the formation material around the fracture reached high water saturations, which would be likely since the vacuum applied at the well pulls water toward the fracture, then liquefaction could take place. In this instance the liquefied material could flow into and deposit within the fracture sand material. This would permanently decrease the permeability of the hydraulic fracture, thus permanently decreasing the flow rate obtained during SVE operation. Well AF-5 and AF-7 may be more susceptible to this problem due to the fact that they are completed at shallow depths as compared to the other fractured wells. Well AF-5 is also located adjacent to a creek that flows heavily during storm events. What exactly happened to wells AF-5 and 7 cannot be known for sure, however, we know that most of the affect on AF-5 was abrupt (Figure 3, following sample event 3). Flow rate and pressure were not logged at a high frequency during the pressure step tests, however, an abrupt decrease in performance of well AF-7 seems to have occurred when the vacuum pressure was increased from 5 to 10 in Hg during phase one testing (Figure 2). These abrupt changes suggest that the problems with these wells are associated with something other than just water infiltration, which would happen over a longer period of time.

Conclusions

The results of this study suggest that hydraulically fractured wells tend to perform better (based on flow rate verses pressure) than conventional wells at the A-014 Outfall site. This evidence further supports conclusions drawn during previous work in M-area. The M-area work showed that hydraulically fracturing wells is an effective means of negating problems associated with well skin, which is most likely a major factor effecting flow rates of conventional wells located in A/M-area. The subsurface pressure distribution data observed during testing (not shown) also suggests that the radii of influence of hydraulically fractured wells are for the most part, significantly greater than that of the conventional well tested in this study.

Data collected during this study show that the performance of hydraulically fractured wells may tend to decrease with time/usage under some field conditions. This type of reaction to SVE has been observed in previous work (Murdoch, 1990), where it was attributed to reduction in vapor phase permeability following in flow of water. Of the five hydraulically fractured wells, one was unaffected (well AF-2), two were affected moderately (wells AF-4 and 8), and two were affected to a large extent and/or showed anomalous behavior (wells 5 and 7) (Figure 6). It is possible that the flow rates at A-area could rebound with additional time. However, rebound during previous studies has occurred soon after dewatering the wells, and this was not observed during the A-area study.

References

- Hall, R.H. 2005. Effects of sand-filled hydraulic fractures during air sparging in saprolite. Master's Thesis. Dept. of Geology, Clemson University.
- Murdoch, L.C. Increased permeability of soils by hydraulic fracturing--a field test, *Proceedings of 21st Ohio River Valley Soils Seminar*, October, 26, 1990.

Appendix B – A-014 Outfall Fracture Enhanced SVE Operational History

Date	Operating Description
Date	
6/11/2007	Initial drawdown testing conducted on all 5 wells at vacuums of 5,
0/11/2007	10, 15 menes rig.
C/12/2007	Re-plumbed solenoid valves - needed to reverse direction to work
0/13/2007	with vacuum instead of pressure.
C/10/0007	Started full operation at maximum vacuum with wells AF-2, -4 and -
6/19/2007	5.
6/22/2007	Solenoid failed on water knock-out tanks and could not be closed to maintain vacuum and flow on the wells. Ordered new valve
0/22/2007	Deigestelled excluse and restarted system at maximum as summer with
6/28/2007	wells AE 2 4 and 5
7/0/2007	Changed wells to AE 7 and 8 with maximum yearsum
//9/2007	Changed wells to AF-7 and -8 with maximum vacuum.
	drawdown tests on each well at vacuums of 5, 10 and 15 inches Hg
	Restarted test system at maximum vacuum with wells AF-2 -4 and -
7/17/2007	8.
	Reconstructed duel phase removal well heads for AF-5 and -7 SVE
7/26/2007	test Unit oil level was low so the system was shutdown.
	Fixed oil problem and refilled unit. Changed wells to AE-5 and -7
	and operated at maximum vacuum High vacuum and low flow
7/27/2007	rates, but water is being removed.
	Changed wells to AF-2 and -4 with maximum vacuum to maximize
8/10/2007	mass removal.
	Oil was being consumed. Shutdown at 10:48 and checked system
8/14/2007	over. Restarted at 16:00
	Oil was being consumed and misting from the stack was occurring.
8/21/2007	Shutdown at 17:15. Ordered Oil.
8/27/2007	Performed maintenance and refilled oil. Restarted at 15:30
	Oil problems still occurring. Shutdown system at 8:50. Found a
9/11/2007	blocked oil return line and cleared it. Restarted at 12:00.
10/24/2007	Area wide power outage caused unit to shutdown at ~15:00.
	The high vacuum from the wells caused the oil to move backward in
	the system and fill and saturate the inlet air filter. Cleaned out and
10/25/2007	restarted. Some rough bearing noises were heard.
	Minor oil leak was occurring. Loose bolts were found on the
	transfer unit connecting the motor and pump. These were tightened
	and the leak was stopped. This was likely a result of the abrupt
	shutdown during the power outage. The unit should not be shutdown under maximum vacuum. This also corrected the poises and
11/12/2007	vibrations that were reported
11/12/2007	The unit went down about 3.00 AM on Sunday morning. The drive
	shaft between motor and the pump has failed. The motor will run
	but the pump is not turning and noise can be heard in the connection
	between the pump and motor. It could be related to the abrupt
12/2/2007	shutdown during the power outage on 10/24/07.

Appendix C – A-014 Outfall Fracture Enhanced SVE Analytical and Operational Data

This appendix contains data collected from the SVE unit (stack sample) and from individual fracture wells. Table C-1 provides the high vacuum SVE unit data including IRPAS (infra-red photo-acoustic spectrometer) concentration data for PCE, TCE and CO₂, vacuum as measured from a mechanical gauge on the unit, flow rate in scfm (standard ft³/min) as measured from a Kurz digital mass flow meter, PCE mass removal rate in lbs/day based on the point flow and concentration data and the wells connected to the SVE unit during those measurements. In the tables, 'nm' indicates the parameter was not measured or recorded.

Tables C-2 through C-6 provide IRPAS concentration, vacuum and flow data for wells AF-2, AF-4, AF-5, AF-7 and AF-8 respectively. These data were collected by isolating individual wells and collecting samples and measurements at the SVE unit. Data recorded from 9/27/07 to 11/13/07 on individual wells AF-2 and AF-4 are suspect and it appears the wells were not completely isolated during the sampling. Figures C-1 through C-5 provide plots of concentration, flow and vacuum for wells AF-2, AF-4, AF-5, AF-7 and AF-8 respectively.

Table C-7 provides gas chromatography (GC) data results from selected stack samples. The GC method used was Savannah River National Laboratory's modified Method 18 for gas analyses. IRPAS and GC results were compared to determine the precision of the IRPAS instrument since it is considered a screening analysis. IRPAS and GC data were in fairly good agreement; however results were approximately 7% low for PCE and 8% low for TCE on the IRPAS instrument. Except for the lower readings of the IRPAS instrument, the correlation between the two analysis methods was good and considered within the error range of the sampling and analysis methods. The IRPAS and GC comparison plots are provided in Figures C-6 and C-7. The total mass removal calculations were based on the IRPAS data that was corrected by 7% for PCE and 8% for TCE since more IRPAS data was collected and provided for more accurate tracking of concentration changes.

Table C-1 – Concentration and Operation Data for SVE Unit							
	DCE	TCE	CO	Venner	Flow	DCE	Walls
	PCE,	ICE,	CO_2 ,	vacuum,	Rate	PCE,	wens
Sample Date Time	ppmv	ppmv	ppmv	in Hg	scfm	lbs/day	Connected
6/9/07 11:30	759	4.5	2800	15.0	88.7	41.0	AF-2, 4, 5
6/9/07 16:15	867	11.2	3010	16.0	86.0	45.4	AF-2, 4, 5
6/12/07 16:00	888	12.3	3150	18.0	71.8	38.8	AF-2, 4, 5
6/13/07 14:20	949	11.8	3400	17.5	79.0	45.7	AF-2, 4, 5
6/19/07 14:30	955	13.9	3600	19.5	61.3	35.7	AF-2, 4, 5
6/20/07 10:40	782	12.6	3650	20.0	58.1	27.7	AF-2, 4, 5
6/20/07 16:40	nm	nm	nm	19.8	59.7	nm	AF-2, 4, 5
6/21/07 9:30	928	8.7	3740	22.0	44.2	25.0	AF-2, 4, 5
6/22/07 8:15	940	9.5	3780	22.0	42.5	24.3	AF-2, 4, 5
6/28/07 14:33	nm	nm	nm	20.0	66.5	nm	AF-2, 4, 5
6/29/07 8:00	880	12.7	3880	21.0	56.3	30.2	AF-2, 4, 5
6/29/07 14:25	nm	nm	nm	21.0	48.3	nm	AF-2, 4, 5
7/2/07 10:30	nm	nm	nm	22.0	42.7	nm	AF-2, 4, 5
7/2/07 10:30	nm	nm	nm	22.0	42.7	nm	AF-2, 4, 5
7/2/07 16:56	nm	nm	nm	23.0	37.0	nm	AF-2, 4, 5
7/3/07 9:30	931	12.5	4020	23.0	37.8	21.4	AF-2, 4, 5
7/3/07 18:00	nm	nm	nm	23.0	38.2	nm	AF-2, 4, 5
7/5/07 8:30	879	12.8	3960	23.0	37.9	20.3	AF-2, 4, 5

Table C-1 - Concentration and Operation Data for SVE Unit

14		Concen	liation ai			LOIII	
	DOE	TOP	60	37	Flow	DOE	XX 7 11
Sampla Data Tima	PCE,	ICE,	CO_2 ,	vacuum,	Rate	PCE,	Connected
	ppinv	ppinv	ppinv	22.0	27.7	105/uay	
7/5/07 10:20	942	12.4	4020	25.0	27.9	10.4	AF-2, 4, 3
7/0/07 14:10	842	12.4	4020	23.0	37.8	19.4	AF-2, 4, 5
7/9/07 10:20	830	14.5	4180	22.5	37.8	19.1	AF-2, 4, 5
7/9/07 16:32	nm	nm	nm	18.0	74.8	nm	AF-7, 8
//10/07 9:30	140	6.1	4170	18.0	73.5	6.3	AF-7, 8
7/11/07 9:30	205	5.8	4400	18.0	73.3	9.2	AF-7, 8
7/12/07 10:32	198	3.9	4450	18.0	71.0	8.6	AF-7, 8
7/12/07 10:45	203	4.0	4590	18.5	67.4	8.3	AF-7, 8
7/16/07 11:30	194	4.6	4220	20.0	nm	nm	AF-7, 8
7/18/07 10:15	441	6.8	4830	18.0	73.8	19.8	AF-2, 4, 8
7/19/07 9:30	413	10.0	4890	18.0	72.0	18.1	AF-2, 4, 8
7/23/07 10:30	382	6.7	4830	19.0	72.4	16.9	AF-2, 4, 8
7/24/07 9:45	375	6.5	4690	19.0	71.6	16.4	AF-2, 4, 8
7/25/07 10:15	412	7.3	5030	19.0	71.2	17.9	AF-2, 4, 8
7/27/07 15:50	182	3.9	5000	26.0	8.0	0.9	AF-5, 7
7/30/07 9:15	370	6.3	4570	25.0	9.7	2.2	AF-5, 7
7/31/07 9:40	385	6.0	4370	25.5	5.2	1.2	AF-5, 7
8/1/07 9:25	320	5.3	4240	26.0	4.4	0.9	AF-5, 7
8/2/07 9:45	329	2.2	4290	26.0	4.8	1.0	AF-5, 7
8/6/07 13:45	395	8.1	4470	26.0	5.7	1.4	AF-5, 7
8/7/07 9:45	375	7.6	4500	26.0	5.6	1.3	AF-5, 7
8/8/07 9:30	393	7.8	4610	26.0	5.8	1.0	AF-5 7
8/9/07 9:30	322	6.8	4180	26.0	6.8	1.1	AF-5 7
8/15/07 11:25	867	18.4	5510	23.0	34.1	18.0	AF-2 4
8/16/07 8:24	898	17.7	5350	23.0	34.5	18.0	$\Delta F_2 / I$
8/20/07 8:41	8/13	18.0	5260	23.0	34.2	17.6	ΔF_2 Λ
8/28/07 10:56	796	17.2	5840	23.0	38.6	18.7	AF 2, 4
8/28/07 10.50	790	17.2	5200	23.0	27.7	16.7	AF 2, 4
8/29/07 9.33	710	17.5	5210	23.0	26.0	10.4	AF-2, 4
0/6/07 0:24	770	1/.1	5450	25.0	26.1	17.5	AF-2, 4
9/0/07 9:34	752	18.5	5450	23.0	25.1	10.5	AF-2, 4
9/1/07 7:52	/51	18.6	5410	23.0	35.1 25.6	16.1	AF-2, 4
9/10/07 8:03	//6	19.6	5400	23.0	35.6	16.8	AF-2, 4
9/11/07 8:15	776	19.4	5360	23.0	35.5	16.8	AF-2, 4
9/12/07 8:42	789	19.9	5370	23.0	35.9	17.3	AF-2, 4
9/13/07 8:14	788	19.9	5480	23.0	35.0	16.8	AF-2, 4
9/17/07 10:01	727	19.2	5650	23.0	33.8	15.0	AF-2, 4
9/18/07 8:46	711	18.4	5580	23.0	33.6	14.6	AF-2, 4
9/19/07 8:38	725	18.7	5690	23.0	33.5	14.8	AF-2, 4
9/20/07 7:48	702	18.2	5500	23.0	33.6	14.4	AF-2, 4
9/21/07 7:57	708	18.4	5650	23.0	33.2	14.3	AF-2, 4
9/24/07 7:51	712	17.8	5650	23.0	32.4	14.1	AF-2, 4
9/25/07 7:58	728	18.0	5730	23.0	32.2	14.3	AF-2, 4
9/26/07 9:05	740	18.5	5760	23.0	32.3	14.6	AF-2, 4
9/27/07 9:17	743	18.7	5790	23.0	32.2	14.6	AF-2, 4
10/1/07 8:33	772	19.3	5770	23.5	32.6	15.3	AF-2, 4

Table C-1 – Concentration and Operation Data for SVE Unit

	DCE	TCE	CO	Voouum	Flow	DCE	Walls
Sample Date Time	FCE,	DDDD	CO_2 ,	in Ho	scfm	FCE, lbs/dav	Connected
10/2/07 8·39	813	20.3	5910	23.5	32.4	16.0	$\Delta F_2 \Lambda$
10/2/07 8:16	700	20.5	5810	23.5	32.4	15.0	ΔE 2.4
10/3/07 8:53	821	20.5	5810	23.0	32.0	16.4	AF 2, 4
10/4/07 8:33	821 821	21.4	5820	23.0	32.0	16.4	AF 2, 4
10/9/07 8.40	031 927	21.0	5800	23.0	32.5	16.2	AF 2, 4
10/0/07 8:32	842	21.5	5860	23.5	32.0	16.5	AF 2, 4
10/9/07 0.41	042 920	21.0	5850	23.5	21.0	16.2	AF 2, 4
10/10/07 8:25	039	21.5	5850	25.0	21.6	10.5	AF-2, 4
10/11/07 8:47	859	22.0	5890	23.0	21.0	10.5	AF-2, 4
10/15/07 8:32	8/4	23.1	6090	23.5	31.0	10.8	AF-2, 4
10/16/07 8:38	884	23.7	6140	23.5	31.9	17.2	AF-2, 4
10/17/07 7:57	885	23.8	6030	23.0	31.9	17.2	AF-2, 4
10/18/07 8:17	881	24.3	5990	23.0	31.8	17.1	AF-2, 4
10/19/07 7:59	904	24.8	5990	23.0	32.8	18.1	AF-2, 4
10/22/07 8:55	909	25.0	6010	23.5	32.9	18.2	AF-2, 4
10/23/07 8:03	918	25.5	6070	23.0	32.8	18.3	AF-2, 4
10/29/07 9:57	849	23.2	6120	23.5	33.6	17.4	AF-2, 4
10/30/07 10:51	837	22.5	6130	24.0	30.9	15.8	AF-2, 4
10/31/07 9:00	833	22.2	6170	24.0	31.3	15.9	AF-2, 4
11/1/07 8:21	828	22.0	6160	24.0	31.0	15.6	AF-2, 4
11/2/07 9:57	821	21.8	6160	23.5	32.0	16.0	AF-2, 4
11/5/07 8:35	821	21.2	6120	23.5	31.3	15.7	AF-2, 4
11/6/07 8:03	819	21.4	6100	23.5	31.6	15.8	AF-2, 4
11/7/07 14:06	831	21.7	6130	23.5	31.4	15.9	AF-2, 4
11/8/07 8:09	nm	nm	nm	23.5	31.2	nm	AF-2, 4
11/12/07 10:33	824	22.8	6080	23.5	30.8	15.5	AF-2, 4
11/13/07 8:24	842	22.5	6050	23.5	31.1	16.0	AF-2, 4
11/14/07 8:29	852	23.2	6080	23.5	31.3	16.2	AF-2, 4
11/15/07 9:15	857	23.5	6100	23.0	31.4	16.4	AF-2, 4
11/16/07 9:11	867	23.4	6050	23.0	31.0	16.4	AF-2, 4
11/19/07 10:12	821	25.3	6060	23.0	30.9	15.4	AF-2, 4
11/20/07 8:18	853	25.6	6110	23.0	31.2	16.2	AF-2, 4
11/26/07 10:11	836	24.2	6000	23.0	31.3	15.9	AF-2, 4
11/27/07 8:47	844	24.3	6060	23.5	31.6	16.3	AF-2. 4
11/28/07 9:17	856	24.3	6070	23.5	31.0	16.2	AF-2, 4
11/29/07 8:34	845	23.8	6080	23.5	31.6	16.3	AF-2, 4
11/30/07 9:25	833	23.5	6070	23.5	30.5	15.5	AF-2. 4

Table C-1 – Concentration and Operation Data for SVE Unit

		1			Flow
Sample Date and	PCE,	TCE,	CO ₂ ,	Vacuum,	Rate,
Time	ppmv	ppmv	ppmv	in Hg	scfm
6/9/07 16:15	1280	7.8	2500	nm	nm
6/12/07 16:02	1230	8.0	2840	nm	nm
6/13/07 14:22	1250	9.0	3430	nm	nm
6/19/07 14:32	1240	8.7	3470	23.0	32.1
6/20/07 10:40	1130	8.5	3660	23.0	29.5
6/20/07 16:40	nm	nm	nm	23.5	28.7
6/21/07 9:32	1030	9.1	3730	23.5	29.1
6/22/07 8:17	1010	9.4	3790	23.5	29.0
6/28/07 14:33	nm	nm	nm	23.5	33.3
6/29/07 8:02	1140	13.0	3690	23.0	31.0
6/29/07 14:25	nm	nm	nm	23.0	29.5
7/2/07 10:30	nm	nm	nm	24.0	24.5
7/2/07 10:30	nm	nm	nm	24.0	24.5
7/2/07 16:56	nm	nm	nm	25.0	25.4
7/3/07 9:32	1090	16.8	3860	24.0	25.3
7/3/07 18:00	nm	nm	nm	24.0	25.0
7/5/07 8:32	1070	17.8	3930	24.0	26.1
7/5/07 16:20	nm	nm	nm	24.0	26.2
7/9/07 10:22	1010	20.8	4070	24.0	26.2
8/15/07 11:20	1010	26.4	4960	24.0	22.6
8/16/07 8:55	1040	22.2	4740	24.0	22.7
8/20/07 8:58	969	22.2	4850	24.5	22.8
8/28/07 11:13	944	20.5	5300	24.0	26.2
8/29/07 10:12	847	22.3	5010	24.0	28.8
8/30/07 8:35	874	20.0	4850	24.0	27.8
9/6/07 9:58	899	20.1	5120	24.0	27.2
9/7/07 8:12	871	22.2	5140	24.0	27.8
9/10/07 8:28	907	22.7	5130	24.0	27.1
9/11/07 8:33	901	21.4	5080	24.0	27.0
9/12/07 8:55	920	23.7	5170	24.0	27.6
9/13/07 8:32	888	22.5	5200	24.0	26.7
9/17/07 10:15	832	22.0	5440	24.0	24.9
9/18/07 9:02	831	22.7	5480	24.0	25.2
9/19/07 8:53	825	21.6	5490	24.0	25.5
9/20/07 8:05	831	22.7	5510	24.0	25.3
9/21/07 8:16	833	22.4	5530	24.0	24.5
9/24/07 8:10	821	21.3	5510	24.0	25.2
9/25/07 8:15	864	23.9	5620	24.0	24.4
9/26/07 9:21	867	23.7	5580	24.0	23.8
9/27/07 9:29*	765	19.7	5720	23.5	30.5
10/1/07 8:44*	885	25.0	5770	24.0	26.2
10/2/07 8:50*	852	22.5	5820	24.0	28.9
10/3/07 8:27*	855	22.5	5790	23.5	29.8
10/4/07 9:06*	864	22.1	5770	23.5	31.1

Table C-2 – Concentration and Operation Data for Well AF-2

					Flow
Sample Date and	PCE.	TCE.	CO ₂ .	Vacuum.	Rate.
Time	ppmv	ppmv	ppmv	in Hg	scfm
10/5/07 8:53*	867	22.7	5800	23.5	30.3
10/8/07 9:05*	872	22.9	5830	23.5	30.1
10/9/07 8:50*	868	22.4	5880	23.5	31.0
10/10/07 8:32*	861	22.1	5880	23.0	30.9
10/11/07 8:59*	886	22.7	5960	23.0	30.7
10/15/07 8:44*	893	23.7	6100	23.5	31.2
10/16/07 8:50*	894	23.7	6120	23.5	31.3
10/17/07 8:05*	904	24.5	6090	23.5	31.0
10/18/07 8:25*	897	24.6	6010	23.0	31.4
10/19/07 8:10*	912	25.2	5970	23.0	32.3
10/22/07 9:06*	925	25.4	6040	23.5	32.6
10/23/07 8:11*	935	26.4	6050	23.5	32.1
10/29/07 10:17*	905	25.4	6220	24.0	31.0
10/30/07 11:01*	855	23.4	6160	24.0	30.0
10/31/07 9:11*	843	22.6	6150	24.0	30.3
11/1/07 8:32*	841	22.6	6110	24.0	30.0
11/2/07 10:08*	844	22.7	6210	24.0	30.5
11/5/07 8:49*	830	21.7	6090	24.0	30.8
11/6/07 8:14*	832	22.1	6100	23.5	30.4
11/7/07 14:17*	941	29.3	6350	24.0	23.3
11/8/07 8:20*	810	22.6	5420	24.0	23.2
11/12/07 10:46*	836	23.5	6040	24.0	30.3
11/13/07 8:35*	853	22.8	6040	23.5	30.7
11/14/07 8:46	968	30.4	6390	24.0	23.4
11/15/07 9:29	972	30.8	6450	24.0	23.5
11/16/07 9:29	987	31.5	6450	24.0	23.0
11/19/07 10:24	908	32.1	6310	24.0	22.8
11/20/07 8:36	986	35.9	6630	24.0	23.2
11/26/07 10:27	969	32.8	6590	24.0	23.4
11/27/07 9:15	966	33.2	6750	24.0	24.0
11/28/07 9:30	962	32.0	6570	24.0	23.1
11/29/07 8:47	944	31.6	6610	24.0	23.4
11/30/07 9:42	943	31.4	6720	24.0	22.5

Table C-2 – Concentration and Operation Data for Well AF-2

* Data is suspect. Valve on AF-4 was likely not closed all the way during sampling.



Figure C-1 – Concentration, Flow and Vacuum Data for Well AF-2

Tuble e 5	Concentrati	on and Oper			
					Flow
Sample Date and	PCE,	TCE,	CO ₂ ,	Vacuum,	Rate,
Time	ppmv	ppmv	ppmv	in Hg	scfm
6/9/07 16:15	1040	2.6	3330	nm	nm
6/12/07 16:04	898	3.2	3280	nm	nm
6/13/07 14:24	970	3.7	3540	nm	nm
6/19/07 14:34	569	2.6	3550	25.0	10.5
6/20/07 10:40	544	2.0	3870	25.0	10.2
6/20/07 16:40	nm	nm	nm	25.0	10.7
6/21/07 10:30	872	3.7	4090	24.8	11.3
6/22/07 8:19	734	5.2	3720	25.0	12.6
6/28/07 14:33	nm	nm	nm	24.5	17.8
6/29/07 8:04	792	4 4	4220	25.0	11.8
6/29/07 14:25	nm	nm	nm	25.5	8.8
7/2/07 10:30	nm	nm	nm	25.0	11.1
7/2/07 10:30	nm	nm	nm	25.0	11.1
7/2/07 16:56	nm	nm	nm	25.0	11.1
7/2/07 0.34	823	4.0	4260	25.0	12.0
7/2/07 19:00	023	4.7	4200	25.0	12.9
7/5/07 18:00	020	6.2	4240	25.0	12.0
7/5/07 16:34	030	0.2	4240	25.0	12.0
7/3/07 10:20	724	7.0	1100	25.0	11.0
//9/07 10:24	/24	/.8	4490	25.0	10.1
8/15/07 11:30	698	12.5	6290	25.0	12.3
8/16/07 8:45	831	16.1	6080	25.0	12.4
8/20/07 8:52	781	17.0	5840	25.0	12.6
8/28/07 11:09	609	11.8	6520	25.0	12.3
8/29/07 10:05	422	7.1	5010	25.0	14.1
8/30/07 8:29	428	6.7	5020	25.0	10.8
9/6/07 9:51	475	8.3	5920	25.5	8.5
9/7/07 8:06	515	8.1	5920	25.5	8.9
9/10/07 8:22	558	9.6	5940	25.5	8.2
9/11/07 8:28	557	9.3	5840	25.5	8.3
9/12/07 8:51	589	8.9	5860	25.5	8.8
9/13/07 8:29	590	9.1	5910	25.0	9.5
9/17/07 10:10	465	9.4	5400	25.0	8.4
9/18/07 8:57	515	9.5	5770	25.0	10.8
9/19/07 8:47	508	9.7	5850	25.0	9.9
9/20/07 8:00	514	9.8	5700	25.0	12.0
9/21/07 8:11	521	9.9	5760	25.0	11.8
9/24/07 8:06	541	10.3	5800	25.0	11.7
9/25/07 8:11	556	10.7	5760	25.0	13.4
9/26/07 9:16	577	10.9	5940	25.0	11.2
9/27/07 9:24*	688	15.6	5770	24.0	23.0
10/1/07 8:39*	717	16.1	5740	24.5	22.5
10/2/07 8:46*	748	17.0	5840	24.0	23.0
10/3/07 8:23*	706	15.3	5700	24.5	19.5
10/4/07 9:02*	734	16.0	5700	24.5	19.6

Table C-3 – Concentration and Operation Data for Well AF-4

	Concentrati	on and Oper			T
					Flow
Sample Date and	PCE,	TCE,	CO ₂ ,	Vacuum,	Rate,
Time	ppmv	ppmv	ppmv	in Hg	scfm
10/5/07 8:49*	749	17.1	5750	24.5	20.7
10/8/07 9:00*	796	18.5	5820	24.0	24.0
10/9/07 8:45*	815	19.9	5790	24.0	27.3
10/10/07 8:28*	818	20.0	5880	24.0	26.3
10/11/07 8:54*	854	21.1	5900	23.5	29.2
10/15/07 8:38*	863	22.0	6060	24.0	28.3
10/16/07 8:46*	873	22.6	6070	24.0	29.4
10/17/07 8:00*	882	23.5	6050	23.5	29.9
10/18/07 8:21*	884	23.7	6000	23.5	30.3
10/19/07 8:06*	877	23.0	5970	24.0	27.2
10/22/07 9:02*	911	24.5	5990	23.5	30.9
10/23/07 8:07*	909	24.8	6030	23.5	30.7
10/29/07 10:12*	727	16.0	5860	25.0	17.8
10/30/07 10:56*	823	21.3	6060	24.0	28.3
10/31/07 9:05*	838	21.9	6160	24.0	30.2
11/1/07 8:26*	825	21.4	6110	24.0	29.9
11/2/07 10:04*	829	21.8	6190	24.0	30.8
11/5/07 8:45*	823	21.1	6090	24.0	30.3
11/6/07 8:09*	821	21.2	6090	23.5	30.7
11/7/07 14:11*	828	21.5	6150	24.0	29.9
11/8/07 8:15*	465	6.2	3590	25.5	7.9
11/12/07 10:42*	817	22.2	6030	24.0	27.8
11/13/07 8:30*	841	21.7	6020	24.0	28.4
11/14/07 8:39	724	10.2	4910	25.5	7.6
11/15/07 9:22	716	10.2	4840	25.5	7.5
11/16/07 9:22	714	9.5	4800	25.5	7.5
11/19/07 10:18	678	10.1	4570	25.5	7.4
11/20/07 8:25	716	10.2	4560	25.5	7.6
11/26/07 10:22	717	9.6	4260	25.5	8.2
11/27/07 9:08	771	10.5	4230	25.5	7.9
11/28/07 9:24	729	9.8	4170	26.0	7.9
11/29/07 8:41	726	9.5	4100	26.0	7.5
11/30/07 9:36	736	10.0	4060	26.0	7.6
					-

Table C-3 – Concentration and Operation Data for Well AF-4

* Data is suspect. Valve on AF-2 was likely not closed all the way during sampling.



Figure C-2 – Concentration, Flow and Vacuum Data for Well AF-4

Sample Date and	PCE,	TCE,	CO ₂ ,	Vacuum,	Flow Rate,
Time	ppmv	ppmv	ppmv	in Hg	scfm
3/8/07 13:34	nm	nm	nm	7.0	18.0
6/9/07 16:15	690	19.3	3460	nm	nm
6/12/07 16:06	605	22.4	3420	nm	nm
6/13/07 14:26	523	29.7	3280	nm	nm
6/19/07 14:36	530	30.0	3510	23.0	36.2
6/20/07 10:40	363	22.3	3490	23.5	26.6
6/20/07 16:40	nm	nm	nm	23.5	26.1
6/21/07 10:32	172	13.5	3090	25.0	6.0
6/22/07 8:21	nm	nm	nm	26.0	1.7
6/28/07 14:33	nm	nm	nm	25.0	18.0
6/29/07 8:06	349	20.1	3720	25.5	8.3
6/29/07 14:25	nm	nm	nm	25.5	8.8
7/2/07 10:30	nm	nm	nm	25.0	10.2
7/2/07 10:30	nm	nm	nm	25.0	10.2
7/2/07 16:56	nm	nm	nm	25.0	2.7
7/3/07 9:36	351	8.5	4000	26.0	3.0
7/3/07 18:00	nm	nm	nm	26.0	2.3
7/5/07 8:36	295	5.4	3820	26.0	2.4
7/5/07 16:20	nm	nm	nm	26.0	3.0
7/6/07 14:10	nm	nm	nm	26.0	3.2
7/9/07 10:26	302	5.6	4510	26.0	3.0

Table C-4 – Concentration and Operation Data for Well AF-5



Figure C-3 – Concentration, Flow and Vacuum Data for Well AF-5

					Flow
Sample Date and	PCE,	TCE,	CO_2 ,	Vacuum,	Rate,
Time	ppmv	ppmv	ppmv	in Hg	scfm
7/9/07 16:32	nm	nm	nm	26.0	2.5
7/10/07 9:32	389	42.5	3870	26.0	2.6
7/11/07 9:30	673	58.7	3960	26.0 26.0	2.3
7/12/07 10:34	1180	74.0	4080		1.6
7/13/07 10:50	516	27.4	3780 26.0	1.4	
7/16/07 11:35	1010	97.7	3640	26.0	nm

Table C-5 – Concentration and Operation Data for Well AF-7



Figure C-4 – Concentration, Flow and Vacuum Data for Well AF-7

Sample Date and Time	PCE, ppmv	TCE, ppmv	CO ₂ , ppmv	Vacuum, in Hg	Flow Rate, scfm
7/9/07 16:32	nm	nm	nm	18.0	74.0
7/10/07 9:34	140	4.9	4150	18.0	74.4
7/11/07 9:30	194	4.4	4350	18.0	73.9
7/12/07 10:36	222	4.5	4430	18.0	71.9
7/13/07 10:55	209	4.1	4530	18.0	72.3
7/16/07 11:40	161	2.8	4750	18.0	nm

Table C-6 – Concentration and Operation Data for Well AF-8



Figure C-5 – Concentration, Flow and Vacuum Data for Well AF-8

Table C-7 – GC Results from the SVE Unit					
Sample Date and	PCE.	TCA.	TCE.		
Time	ppmv	ppmv	ppmv		
6/19/2007 14:45	976.9	1.3	14.0		
6/20/2007 10:45	840.0	1.1	13.5		
6/21/2007 9:40	1047.2	0.5	8.8		
6/29/2007 8:45	918.5	1.0	12.6		
7/3/2007 9:30	915.6	0.8	15.3		
7/9/2007 13:30	735.7	0.9	14.8		
7/10/2007 9:45	132.8	0.3	6.5		
7/12/2007 10:30	189.5	0.3	4.4		
7/13/2007 10:45	197.3	0.4	4.5		
7/16/2007 11:30	209.5	0.4	4.9		
7/18/2007 10:15	437.6	0.4	7.6		
7/23/2007 10:30	391.2	0.4	9.1		
7/25/2007 10:15	390.6	0.4	7.3		
7/30/2007 9:15	353.7	1.3	5.8		
7/31/2007 9:40	388.5	1.7	6.2		
8/2/2007 9:45	321.4	1.2	6.1		
8/6/2007 13:45	401.1	1.6	8.4		
8/7/2007 9:45	370.0	1.4	7.1		
8/8/2007 10:15	416.4	1.6	8.3		
8/10/2007 13:00	327.3	1.5	6.8		
8/16/2007 8:27	920.7	0.8	17.6		
8/28/2007 10:59	911.3	0.8	19.5		
8/30/2007 8:19	772.8	0.8	18.5		
9/7/2007 7:56	817.3	0.8	20.5		
9/10/2007 8:08	774.6	0.8	21.9		
9/13/2007 8:17	690.9	0.9	23.3		
9/18/2007 8:48	775.8	0.9	20.5		
9/21/2007 8:00	818.7	0.8	18.9		
9/24/2007 7:54	777.6	0.8	20.0		
9/27/2007 9:19	831.5	0.9	20.7		
10/2/2007 8:41	878.6	1.1	21.1		
10/5/2007 8:43	871.2	1.2	23.2		
10/8/2007 8:55	924.4	1.4	25.0		
10/11/2007 8:51	1127.9	1.6	26.6		
10/16/2007 8:43	1004.0	2.0	28.5		
10/19/2007 8:02	1037.0	2.0	24.8		
10/29/2007 10:01	1115.5	2.2	28.1		
11/2/2007 10:00	1030.9	1.8	24.1		
11/5/2007 8:40	806.2	1.8	22.9		
11/12/2007 10:36	882.6	2.3	22.7		
11/16/2007 9:14	951.9	2.0	25.4		
11/19/2007 10:30	766.1	2.1	23.0		
11/26/2007 10:15	858.1	2.6	25.6		
11/30/2007 9:29	8597	2.4	24.5		



Figure C-6 – Comparison of IRPAS and GC Analytical Results for PCE



Figure C-7 – Comparison of IRPAS and GC Analytical Results for TCE