Boosted Fast Flux Loop Alternative Cooling Assessment

Glen R. Longhurst Donna Post Guillen James R. Parry Douglas L. Porter Bruce W. Wallace

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ABSTRACT

The Gas Test Loop (GTL) Project was instituted to develop the means for conducting fast neutron irradiation tests in a domestic radiation facility. It made use of booster fuel to achieve the high neutron flux, a hafnium thermal neutron absorber to attain the high fast-to-thermal flux ratio, a mixed gas temperature control system for maintaining experiment temperatures, and a compressed gas cooling system to remove heat from the experiment capsules and the hafnium thermal neutron absorber. This GTL system was determined to provide a fast (E > 0.1 MeV) flux greater than 1.0E+15 n/cm2-s with a fast-to-thermal flux ratio in the vicinity of 40. However, the estimated system acquisition cost from earlier studies was deemed to be high. That cost was strongly influenced by the compressed gas cooling system for experiment heat removal. Designers were challenged to find a less expensive way to achieve the required cooling. This report documents the results of the investigation leading to an alternatively cooled configuration, referred to now as the Boosted Fast Flux Loop (BFFL). This configuration relies on a composite material comprised of hafnium aluminide (Al₃Hf) in an aluminum matrix to transfer heat from the experiment to pressurized water cooling channels while at the same time providing absorption of thermal neutrons. Investigations into the performance this configuration might achieve showed that it should perform at least as well as its gas-cooled predecessor. Physics calculations indicated that the fast neutron flux averaged over the central 40 cm (16 inches) relative to ATR core mid-plane in irradiation spaces would be about 1.04E+15 n/cm2-s. The fastto-thermal flux ratio would be in excess of 40. Further, the particular configuration of cooling channels was relatively unimportant compared with the total amount of water in the apparatus in determining performance. Thermal analyses conducted on a candidate configuration showed the design of the water coolant and Al-Hf alloy heat sink system is capable of maintaining all system components below their maximum temperature limits. The maximum temperature of this conduction cooling system, 224.2°C (435.6 °F) occurs in a small, localized region in the heat sink structure near the core mid-plane. The total coolant flow rate requirement for this configuration is 207 L/min (54.7 gpm). The calculated Flow Instability Ratio and Departure from Nucleate Boiling Ratio for this configuration under nominal conditions are 6.5 and 8.0, respectively, which safely exceed the minimum values of 2.0. Materials and fabrication issues inspection revealed that the neutron absorber would probably best be made from powdered Al₃Hf mixed with aluminum powder and extruded or hot isostatically pressed. Although Al₃Hf has not been specifically studied extensively, its mechanical and chemical properties should be very much like Al₃Zr, which has been studied. Its behavior under irradiation should be very satisfactory, and resistance to corrosion will be investigated to a limited extent in planned miniplate irradiation tests in ATR. Pressurized water systems needed to effect heat removal are already available in the ATR complex, and mixed gas temperature control systems needed to trim experiment temperatures have been engineered and need only be fabricated and installed. In sum, it appears the alternately cooled configuration arrived at can be very successful. The cost estimate for this configuration indicates total project costs between \$50M and \$75M, including more than \$11M for neutron charges, which is a saving of 25% over the previous configuration.

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	ACRONYMS	
ATR	Advanced Test Reactor	
BFA	Booster Fuel Assembly	
BFFL	Boosted Fast Flux Loop	
CD-0	Critical Decision 0 (mission need establishment)	
DNBR	Departure from Nucleate Boiling Ratio	
FIR	Flow Instability Ratio	
GTL	Gas Test Loop	
HFRI	High Flux Isotope Reactor	
ITV	Irradiation Test Vehicle	
LANSCE	Los Alamos Neutron Science Center	
MTS	Materials Test Station	
NW	Northwest	

1.0 BACKGROUND

In 2004, a Mission Need (CD-0) was established for an augmentation to an existing nuclear facility that would enable the testing of advanced reactor fuels and materials under fast-flux irradiation conditions.[1] The Gas Test Loop (GTL) Project was established at the Idaho National Laboratory in response to that need. Technical and Functional Requirements[2] were developed for a system that would accomplish the mission identified in the Mission Need document.

A survey was subsequently performed of a large number of reactors and accelerators where such a capability could be developed.[3] After a preliminary review, five facilities were considered for a more detailed evaluation. These included the JOYO fast reactor in Japan, the BOR-60 in Russia, the High Flux Isotope Reactor (HFIR) at Oak Ridge National Laboratory, and the Advanced Test Reactor (ATR) at the Idaho National Laboratory as well as the proposed Materials Test Station (MTS) at the LANSCE accelerator at Los Alamos National Laboratory. The conclusion of this investigation was that the facility best suited to meeting the established functional requirements was the ATR.

The conceptual design of the GTL, based on using one of the ATR corner lobes, was initiated in 2005. The conceptual design report[4] showed that of the more than 20 different configurations examined, the design with the best performance was the one shown in Figure 1 below.

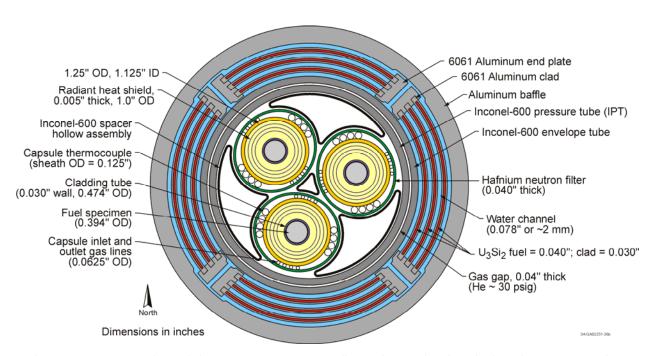


Figure 1. Cross section of the Gas Test Loop configuration arrived at during the conceptual design activity.

Main features of that design included the booster fuel located inside the lobe flow baffle, a double in-pile tube pressure boundary, three experimental positions each surrounded by a hafnium filter for capturing thermal neutrons, and two associated gas systems. The first gas

system was for temperature control through a variable conductance gas gap. That gap is indicated in Figure 1. The second was a pressurized helium system for removing heat generated in the experiment targets and the hafnium filter. It passed through the central region of the experiment chamber, as shown in Figure 1, but much of the central region volume was filled with a gas displacer, allowing the cooling gas to flow over the hot surfaces at much higher velocities and thus be more efficient in removing the heat.

The overall system configuration is shown in Figure 2, illustrating the elements of the gas cooling system and the other significant components of the design.

The estimated cost of the GTL system was between \$85M and \$100M. While that is relatively expensive for a fuel development program to support, it is much less than the cost of a new fast-flux test reactor. It could also be brought on line in approximately 5 or 6 years, which is much faster than a new test reactor can be built. It would provide a fast-flux test capability in the time before a fast-flux research reactor could be built. That notwithstanding, support for the GTL concept was sparse, in part because of its relatively high cost.

A review of the cost estimate basis showed that approximately 30% of the total system cost was associated with the gas systems. It was supposed that if a way could be found to remove the heat from the experiment chamber that did not involve the pressurized gas system, the overall project cost could be reduced substantially, and the concept would be more attractive to potential users.

This report documents the results of the investigation into an alternately cooled version of the GTL. For definiteness, this system is referred to as the Boosted Fast Flux Loop (BFFL). In the sections that follow will be presented the methods used in seeking for an alternately cooled approach, the results of that search, physics and thermalhydraulic analyses to assess the functional viability of the concept arrived at, materials and fabrication concerns, and a discussion of the cost impact this configuration may have on the establishment of a fast-flux test capability in the ATR.

2.0 APPROACH

This section presents the approach used in arriving at an alternately cooled concept. It begins with the issues faced, the objective definition, and bases used for concept deliberations.

2.1 Issues

Conflicting technical requirements led to the selection of pressurized gas as the experiment coolant in the original GTL design. One requirement is that in order to have a good fast-to-thermal neutron flux ratio, there must not be any significant neutron thermalizer between the hafnium filter and the experiment target. Water, which is typically used as a heat sink in the ATR, is a strong thermalizer. Another requirement is that we meet the fast flux intensity goal. This means substantial heating of the targets, particularly if they are fuel targets, as well as a large amount of heat being generated in the hafnium filter from the (n,γ) neutron absorption reactions. That heat must be carried away to limit experiment temperatures. A final consideration is ATR operating safety and the concern that exists about use of liquid metals and molten salts in the ATR reactor.

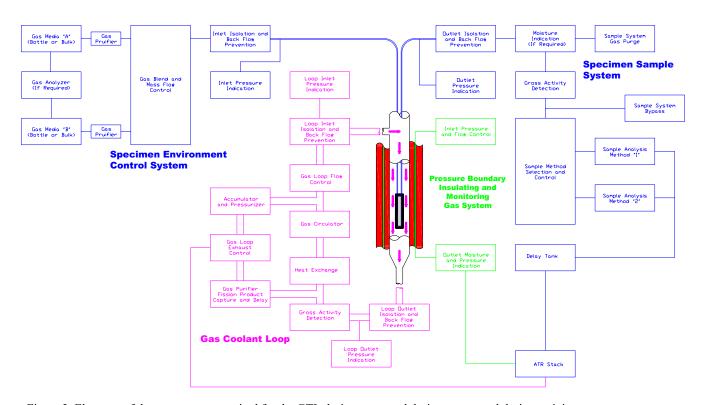


Figure 2. Elements of the gas systems required for the GTL design generated during conceptual design activity.

2.2 Study Objective

The specific objective of this study was to see if it is possible to adequately cool the experiments using some means of experiment cooling other than pressurized gas.

2.3 Study Bases

To provide a point of departure for this study, it was assumed, that BFFL will be located in an ATR large flux trap and retain the booster fuel configuration shown in Figure 1. This booster fuel configuration was determined through rather extensive comparisons to provide the most optimal generation of the high flux intensity needed to achieve BFFL performance targets.

This assumption fixed the outer diameter of the in-pile tube that will be needed to contain the experiment. That diameter is 9.128 cm (3.593 inches). If an in-pile tube provides a pressure boundary for the primary coolant, it must be a double boundary, and existing engineering codes and standards will need to be applied in its design.

It was assumed that the primary BFFL users will be developers of advanced fuels and materials such that typical experiments will consist of fuel specimens, nominally 1 cm in diameter and with axial heating rates up to 2.3 kW/cm (70 kW/ft) with a total heat load from test articles to be up to 200 kW (see Ref. 2). Cooling needed to be capable of maintaining test article surface temperatures at 500°C but the cooling system should be compatible with 1,100°C as a possible test article surface temperature (if it is practical).

For economy of operation, the original design had 3 parallel test columns. While this was desirable to maintain, this study also looked at a different number of test columns to evaluate feasibility.

While hafnium is a very attractive thermal neutron filter because of the many sequential absorption reactions it undergoes, it was not required that it be maintained as the filter material. However, some kind of filter was required to keep the fast-to-thermal ratio greater than 15.

There are specific guidelines as to material limitations in the ATR [5] Potential designs should be screened against materials acceptance criteria to be sure that no design would compromise ATR operational safety.

2.4 Path Forward

The first step was to become creative and synthesize alternative configurations that may provide the needed performance. This was aided by a review of work that has been done in the past, as documented in Ref. [4] and other project documents and files. Concept synthesis was initiated in a brainstorming session.

The plan was that concepts developed should then be reduced to sketches with specified dimensions and materials.

Neutronics codes such as MCNP should then be exercised to determine flux levels achieved with those designs and material heating rates.

Thermal/hydraulic analyses should be performed on the designs with appropriate heating rates and heat transfer parameters to determine the ability of each design to meet the required

performance. Analysis tools that were thought to be particularly useful for thermal/hydraulic analyses include RELAP-5 and ABAQUS.

Findings of these investigations were discussed in follow-up meetings. While some variations in design were recommended, it was not necessary to initiate further iterations of the basic design process.

2.5 Discussion Results

The first meeting to synthesize a new concept was held on May 9, 2007. After reviewing the meeting objectives, participants first reviewed the current design and the considerations that led to it.

They discussed possible cooling schemes. There are only two ways to get the heat out of the test specimens and the hafnium filter: convection and conduction. Radiation can play a non-trivial role at high target temperatures.

Convection requires a fluid. A number of fluids were discussed including molten metal, molten salt, gases other than He, organics, and water. It was supposed that the cost of molten metal or molten salt systems would be comparable to or greater than that of pressurized gas systems. Furthermore, there are safety concerns about putting into the reactor any fluid that could react with the primary coolant, and it did not appear practical to make use of a fluid that must be kept hot to prevent structural damage. When working with gases, convective performance is the product of mass flow rate and specific heat. The molar specific heats of most gases are not very different and don't really change until high temperatures excite rotation and vibration modes, which do not exist in noble gases. The volumetric specific heat is increased by pressurization. Hence the way to increase cooling is to increase flow. High temperature gas reactors (Ft. St. Vrain for example) have experienced major problems with circulators and other components. Even though there are a few gas-cooled reactors operating outside the U.S., it seemed prudent to look elsewhere than gas convection for this application. There may be support from other programs or projects to participate in developing gas system technology that could be used, but they were not to be counted on.

The most viable liquid for use in ATR seemed to be water, where a major concern is fast neutron thermalization.

Basic problems with conduction have included getting the heat from the experiment specimens and the hafnium out through the pressure boundary. This is driven in large measure by conduction gaps at material interfaces. This is usually mitigated by increasing surface area available for heat transfer and providing thermal bonding agents.

3.0 NEW APPROACH

With the above points in mind, it was suggested that we may be able to use a novel approach that involves both conduction and water convection. The first implementation of this concept is shown graphically in Figure 3.

The key to this approach is the use of a novel material for the basic fill of the test space. This would be a hafnium-aluminum composite, manufactured from powder of either hafnium, hafnium aluminide intermetallic, or hafnium oxide, mixed with aluminum powder and pressed or

extruded. This material would retain the high thermal conductivity of aluminum but have the thermal neutron absorption properties of hafnium. We would have to determine what the best hafnium loading would be, but from a materials perspective, there should be no major technological barrier to making it.

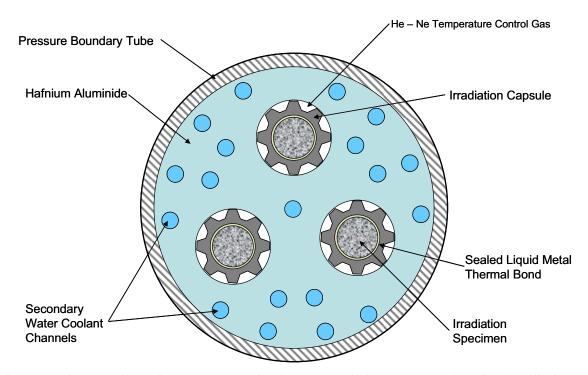


Figure 3. First configuration of a pressurized water cooled concept for fast flux irradiation testing.

An early concept was that the hafnium aluminum would be penetrated by small (~6-mm) cooling channels of pressurized water from a secondary cooling system. These cooling channels would need to be located sufficiently far from the irradiation capsules that the hafnium in the matrix would provide adequate absorption of thermal neutrons born in the water channels. Earlier analysis showed that as little as 1-mm of solid Hf would provide adequate filtering. Therefore, if the Hf in the matrix were 10% atomic fraction, then 10 mm spacing should be adequate. A key to performance for heat removal is the high thermal conductivity of the aluminum in the hafnium aluminum. This could carry the heat to the cooling channels with only small temperature gradients, resulting in more or less circumferentially uniform cooling of the experiments.

It was pointed out that there is already a task in progress to restore the pressurized water system in the 2A cubicle, as part of the INL master contract agreement. There is no particular customer identified for this system, except that it is to be used to restore testing capability to the ATR. Another, possibly less expensive option is to make use of the pressurized water system already serving the ATR NW Lobe.

Another important issue is the transfer of heat to the hafnium aluminum absorber. We supposed that the fuel would be thermally bonded to the experiment capsule using molten metal, such as Na or Li. This is done routinely in other ATR fuel experiments. The capsule will need to be

made of a more or less refractory metal, such as Inconel to withstand the high temperatures of anticipated fuel experiments. At issue, then, is heat transfer from the capsule to the hafnium aluminum absorber and the ability to apply temperature control. Shown in Figure 3 is a configuration only representative of the approach. The basic conduction would be provided through thick fins or lands that would have a close tolerance fit to the aluminide. Trim in conductance would be provided by a standard He – Ne gas mixture that would be slowly flowed through the gaps (shown exaggerated in thickness in Figure 3) between the fins or lands. Considerably more thermal analysis was needed to determine land width and number, gap spacing and such things. If needed, the fins or lands could fit into conforming grooves in the hafnium aluminum, like a spline gear set, to provide greater area for heat transfer to take place. Mechanical issues of separating the temperature control gas mixture from the secondary coolant water would need to be dealt with, but should not be overly difficult. It was also noted that the architecture of a multi-channel temperature control gas system is being designed by the TMIST project and the BFFL would only need to populate the basic framework with specific mass flow controllers, etc. to have a functioning system. Another option is the restoration of the Irradiation Test Vehicle (ITV) [6] gas temperature control system.

An interesting and novel suggestion was that if heat transfer from the capsules to the hafnium aluminum is rate limiting, it may be possible to make use of a heat-pipe effect to distribute heat vertically along the experiment such that it could enter the hafnium aluminum in regions well above or below the core mid-plane where heating will be much less. It is likely that many experiments would only make active use of the few inches above and below the mid-plane to achieve vertical flux uniformity in the test specimens.

3.1 Configuration Development

As thermal and physics analyses were conducted, three additional cooling configurations were examined. These are shown in Figures 4 to 6. A fourth additional concept is a combination of the annular ring and four-hole concepts (Figures 4 and 6).

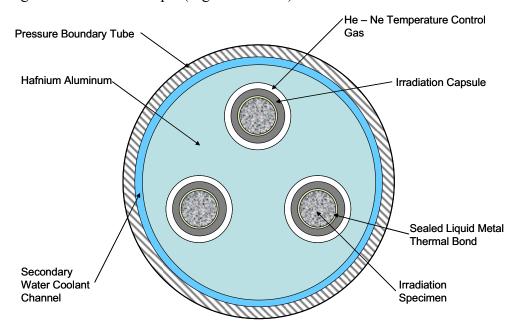


Figure 4. Annular ring cooling concept

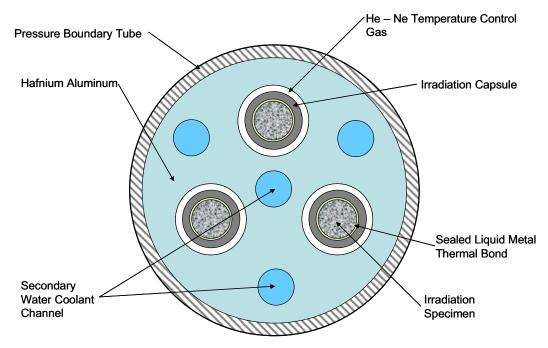


Figure 5. Four hole cooling concept.

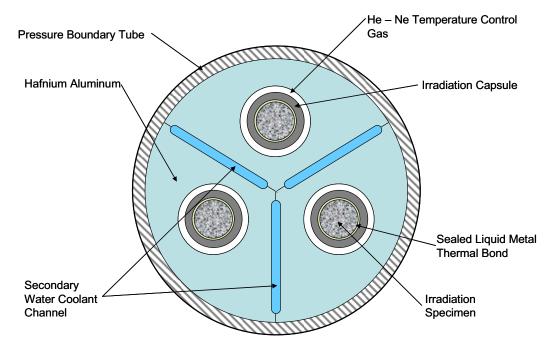


Figure 6. Radial vane cooling concept.

3.1 Analysis Results

With basic configurations in mind, the next step was developing and exercising numerical models of these structures to examine physics issues of criticality and neutron flux intensity, and heating rates for the targets and neutron absorbing material.

3.1.1 Physics

Physics analyses were performed with the objective of determining the optimum hafnium content in the aluminum neutron absorber and determining heating rates in the structure. The first physics analysis was performed on a configuration identical to that of Figure 1, used as a baseline or starting point. That model had the following features relative to previous ones that had been used.

- Removed Hf filter from the outside of the pressure tube, increasing envelope tube thickness to compensate.
- Changed Booster Fuel Assembly (BFA) plate loadings to 1.7, 3.0, and 4.8 gU/cc.
- Reduced thickness of inner plate fuel meat from 1.52mm (0.060 inch) to 1.01 mm (0.040 inch).
- Added 1mm Inconel 600-clad Hf ellipse around each experiment tube. (The ellipses are 0.5-mm Hf with 0.25 mm thick clad inside and out.)
- Replaced the material for the envelope and pressure tubes with Inconel 600.
- Replaced Al spacers with hollow (0.5-mm/0.020-inch wall) Inconel 600.
- Adjusted envelope and pressure tube dimensions to be closer to minimum required thicknesses both are 0.125in (0.2921cm).
- Experiment tubes were equally spaced on a 1.795" circle.
- BFA has 2-mm (0.079-inch) gap between sideplates, 5.76-mm (0.227-inch) sideplates, and 2.41-mm (0.095-inch) gap between sideplate and fuel meat.
- Added gas lines and thermocouple tubes in test region.

The cross section of that model as implemented in MCNP is shown in Figure 7.

MCNP5 Version 1.40, a monte-carlo neutronics code, was used in the analysis.[7] Its use has been validated at the INL. It was run on the Helios computer cluster at INL. Reactor lobe powers were assumed as shown in Table 1. This is the same reference case used in prior calculations using this baseline GTL configuration (Figure 1).

Table 1. ATR power distribution assumed for initial physics calculations.

Lobe	Power (MW)	Fraction
NW	52.36	37.4%
NE	15.21	10.9%
С	33.68	24.1%
SW	20.50	14.6%
SE	18.25	13.0%
Total	140	100.0%

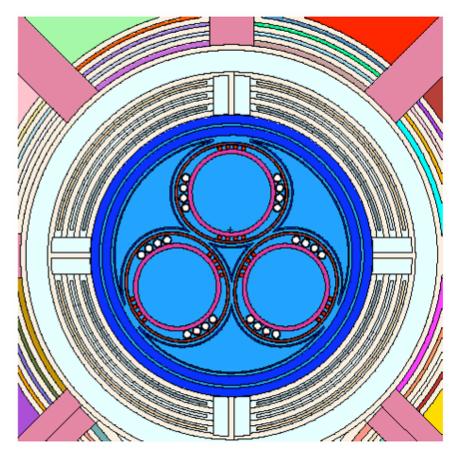


Figure 7. MCNP model of the reference configuration, used to establish a physics baseline.

This baseline configuration was found to have a fast flux (E . 0.1 MeV) in the experiment volumes of 1.03E+15 n/cm2-s and a fast-to-thermal ratio (E > 0.1 MeV / E < 0.68 eV) of 43.

The model of Figure 7 was then modified as follows:

- Replaced interior structures in the target regions with solid aluminum structures
- Started with solid aluminum in the spaces between the test chambers and only helium in the gas gap (no experiments, thermocouples, etc.)
- No Hafnium sleeves on the experiment chambers

The modified MCNP model is shown in Figure 8. Among the parameters calculated were the fast-to-thermal ratio and the fast flux intensity averaged over the central 40 cm (16 inches) of the core height. Figure 7 shows how those quantities vary with hafnium content (number fraction) in the aluminum.

These calculations gave a fast flux of 1.04E+15 n/cm2-s and a fast-to-thermal ratio of 20.4 even with no hafnium in the aluminum filler. The high fast-to-thermal ratio appears to be a consequence of having the booster fuel close to the experiment chambers and the absorption of thermal neutrons by the Inconel 600.

The model of Figure 8 was then modified by adding in increments hafnium to the aluminum filler surrounding the test spaces. Results are shown in Figure 9.

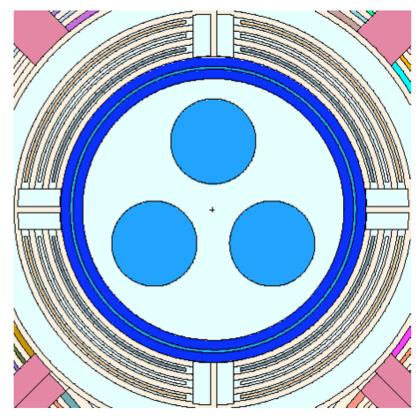


Figure 8. First modification to MCNP model to explore hafnium content effects on performance.

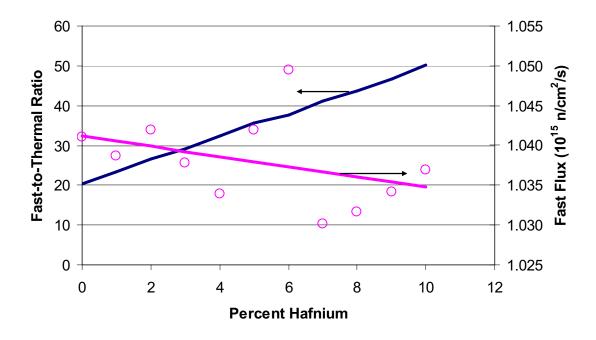


Figure 9. Sensitivity of fast-to-thermal ratio and fast flux intensity to hafnium content in the aluminum central filler piece (absorber).

It is intuitive that the greater the presence of hafnium in the aluminum, the greater would be the fraction of thermal neutrons that are removed. It is likewise intuitive that the greater the presence of hafnium, the fewer neutrons generally will enter the target regions. The data points in the fast flux results show considerable scatter about the best fit line. This scatter is a consequence of numerical convergence error in the code, but the line shown should be consistent with the actual flux.

Heating rates in the hafnium-aluminum were also calculated as a function of the hafnium concentration in the absorber. These rates are shown, averaged over the central 40 cm (16 inches) of core height, in Figure 10. The actual vertical heat profile will be a chopped cosine function, following the neutron flux intensity. The heating rate, a measure of neutron absorption, appears to saturate at about 6-7% hafnium, which suggests that may be an optimum hafnium loading. Volumetric heating density continues to increase with increasing hafnium loading as more and more thermal neutrons are captured because of the greater abundance of hafnium in the absorber. This appears to saturate at a hafnium concentration of 12% (1/e value 3.4%) at a heating density of 52 W/cm³, when effectively all of the thermal neutrons are absorbed.

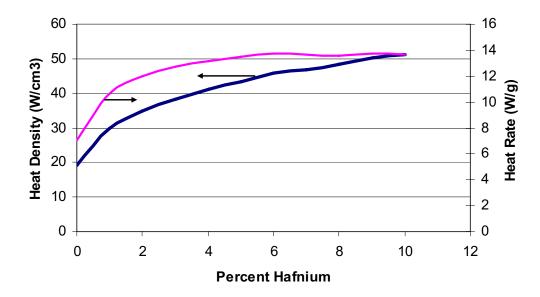


Figure 10. The heating rate and heat density of the hafnium-aluminum averaged over the central 40 cm (16 inches) of the core height.

A second series of calculations sought to evaluate the extent to which the amount of water in the cooling channels would influence the performance of this configuration. These calculations were performed on each of the configurations shown in Figures 4 through 6. Results are plotted in Figure 11 as a function of the cross sectional area of water in the figures. It did not seem to make much difference which configuration was used in comparison with the total amount of water in the system.

It is clear from Figure 11 that the more the water in the system, the less is the fast neutron flux. This is a natural consequence of the thermalizing effect of the water on neutron energies. The fast-to-thermal ratio also declines with increasing water in the system. Again, more water

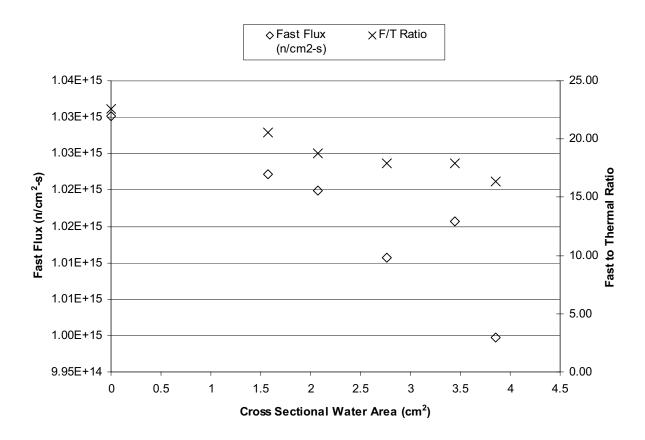


Figure 11. Effect of water presence on the performance of the hafnium-aluminum thermal neutron absorber.

reduces the number of fast neutrons available because of thermalization. Absorption of thermal neutrons is effectively constant.

It is concluded from these calculations that it is possible to achieve the same level of performance in the alternatively cooled concept as was estimated in the original gas-cooled concept, namely a fast flux in excess of 1.0E+15 n/cm2-s and a fast-to-thermal ratio in the vicinity of 40. It appears further that a hafnium atom fraction in the vicinity of 7% may be optimal. Finally, the configuration of the water cooling channels does not appear to make much difference in the neutronic performance in comparison with the amount of water inside the pressure boundary.

3.1.2 Thermal/hydraulic Analysis

3.1.2.1 Model Setup and Boundary Conditions

A thermal hydraulic model of one BFFL configuration was constructed and evaluated to determine whether the proposed configuration is capable of cooling a set of experiments located in the NW Lobe of the ATR. A model was created using ABAQUS version 6.6-3 [8] to determine component temperatures. The conductive cooling system consists of the following components:

• Conduction heat sink and thermal neutron absorber

- Coolant channels
- Envelope tube
- Pressure tube
- Helium gas gap
- Oxide layers

Figure 12 illustrates the BFFL configuration that was analyzed. A conduction heat sink fabricated from a Al-7 wt% Hf alloy serves a dual role as a neutron filter and a medium to conduct heat away from the experiments. The heat sink surrounds three 3.17-cm (1.25-inch) diameter experiment tubes situated on a 4.56-cm (1.795-inch) circle. Four 6.35-mm (0.25-inch) diameter water coolant channels are located within the heat sink. Three of the water channels are positioned 120 degrees apart on a 3.09-cm (1.22-inch) circle and the fourth water channel is located at the center. A 0.762-mm (0.030-inch) water annulus is located between the heat sink and the pressure tube. Oxide layers (12.7 μ m, 0.0005 inch thick) are assumed to be present on the surfaces of the heat sink exposed to the water coolant. An envelope tube (9.591-cm, 3.776-inch ID; 10.226 cm, 4.026 inch OD) surrounds the pressure tube (8.753-cm, 3.446-inch ID; 9.388-cm, 3.696- inch OD) with a 1.016-mm (0.040 inch) helium gas gap in between for the purpose of leak detection monitoring. Both tubes are constructed of 3.175-mm (1/8-inch) thick Inconel-600.

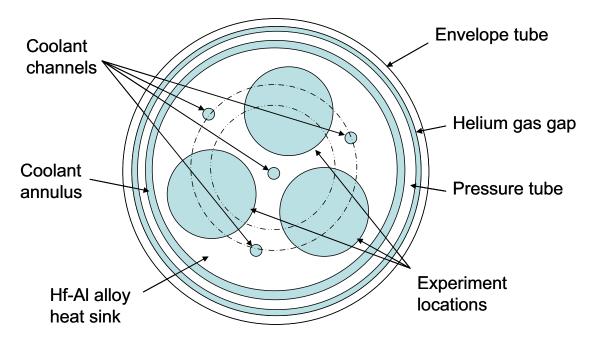


Figure 12. Proposed BFFL Conduction Cooling Configuration (not to scale).

The envelope tube, pressure tube and oxide layers were modeled as shells. The water channels, water annulus and heat sink were modeled as 3D solids. The 3D model is comprised of 115,592 elements. All components in the model have a length of 1.219 m (48 inches).

Coolant water to the annulus and cylindrical water channels is supplied by the 2A pressurized water loop at 12.4 MPa (1800 psia). The inlet water temperature and component initial temperature are assumed to be 110°C (230 °F). Coolant flows through the annulus at a flow rate

of 90 L/min (23.8 gpm) and through the water holes at 116.9 L/min (30.9 gpm). The annulus and water channel mass flow rates are specified as $0.687~kg/s-cm^2$ (9.76 lbm/s-in²) and $1.464~kg/s-cm^2$ (20.81 lbm/s-in²), respectively. The total volume of water is $4.076~x~10^{-4}~m^3$ (24.87 in³), with 0.2532~L (15.45 in³) in the annulus and 0.1544~L (9.422 in³) in the four cylindrical water channels.

Results from RELAP5-3D [9] were used to specify the convection boundary condition at the outside of the envelope tube. The external surface of the envelope tube is cooled by ATR primary coolant flowing at a velocity of 13.59 m/s (44.6 ft/s) with an average coolant temperature of 82.2°C (180 °F).

To facilitate specification of heat loads, the geometry was partitioned into 12 axial sections, with six 10.16-cm (4-inch) sections above and below the core mid-plane. The following calculation shows how the axial power profile was calculated.

Normalized power curve based on ATR axial flux profile.

i := 0...5

Eight axial segments on each side of core centerline

 $\Delta x := 4.0 \text{ in}$

Length of each segment

$$x_i := (i + 0.5) \cdot \Delta x$$

Distance from core centerline (center point of each axial segment)

$$x = \begin{pmatrix} 2 \\ 6 \\ 10 \\ 14 \\ 18 \\ 22 \end{pmatrix}$$
 in

$$P_{norm_{\hat{i}}} := 1.41 \cdot cos \left(0.058 \frac{1}{in} \cdot x_{\hat{i}} \right)$$

Normalized power in each segment

$$P_{norm} = \begin{pmatrix} 1.401 \\ 1.325 \\ 1.179 \\ 0.97 \\ 0.709 \\ 0.41 \end{pmatrix}$$

Table 2 lists the average heat loads for the system components. A surface heat flux representing the thermal loads from the experiments were applied at the three cylindrical surfaces inside which the experiments will be located. Body heat fluxes to account for gamma heating were applied in the structural components. The average heat loads were multiplied by the power profile calculated above and applied symmetrically to the six segments above and six segments below the core mid-plane. Detailed calculations for the model components are provided in Appendix A. The applied loads are higher near the core mid-plane, and decrease with distance from the core mid-plane.

Table 2. Average heat loads for each model component.

Component	Average Heat Load (kW)	Heat Flux Condition
Experiment Tubes	70 each/210 total	Surface
Heat Sink	40.3	Body
Pressure Tube	58.32	Body
Envelope Tube	70.5	Body
Cylindrical Water Channels	3.741	Body
Water Annulus	6.135	Body

An additional case was analyzed which was identical to the one just described except that an additional surface heat load from each of the three experiment chambers of 58 kW (174 kW total) was assumed. This *alternate configuration* may be representative of leaving the hafnium filter sleeves of Figure 1 in place or of additional heating from the irradiation targets themselves.

3.1.2.2 Results

The results from the ABAQUS base case thermal analysis are shown in Figures 11 through 18.

Figure 13 shows the temperature distribution on the inside surface of the envelope tube. The maximum temperature (116.4°C, 239.7 °F) in the envelope tube occurs in the mid-core region at the inner diameter. The outer diameter of this component is convectively cooled by ATR primary coolant, whereas the inner diameter is effectively insulated by the 1.016-mm (0.040-inch) helium gap, which causes the temperatures to be higher on the inner surface.

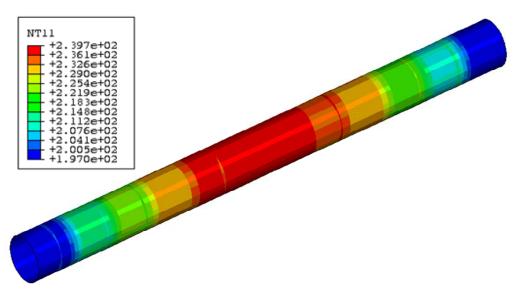


Figure 13. Temperature distribution (°F) on inner surface of envelope tube (base case).

Figure 14 shows the temperature distribution on the outer surface of the pressure tube. The maximum temperature $(160^{\circ}\text{C}, 320^{\circ}\text{F})$ in the pressure tube occurs just below the mid-core region. The outer surface is hotter than the inner surface, due to the presence of the helium gas gap at the outer surface, which serves to insulate. The inner surface is convectively cooled by pressurized water coolant flowing through the annulus between the pressure tube and heat sink. A 120 degree section cutaway is shown – the sections are symmetric.

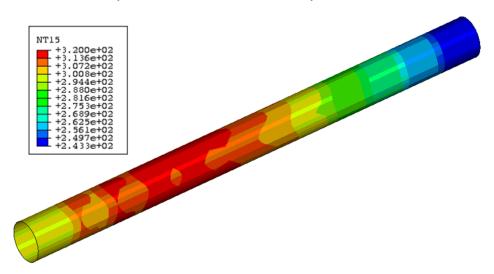


Figure 14. Temperature distribution (°F) on outer surface of pressure tube (base case).

Figures 15 and 16 show the temperature distribution in the hafnium aluminum absorber. The three large holes in Figure 15 are locations of the experiment tubes and the four smaller holes contain the water coolant channels. From the cutaway view shown in Figure 16, it can be seen that the temperature in the heat sink reaches a maximum of 224.2°C (435.6 °F) in the regions between the experiment tubes near the core mid-plane.

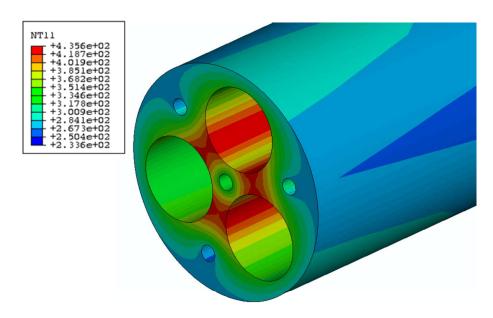


Figure 15. Radial temperature distribution (°F) in the heat sink (base case).

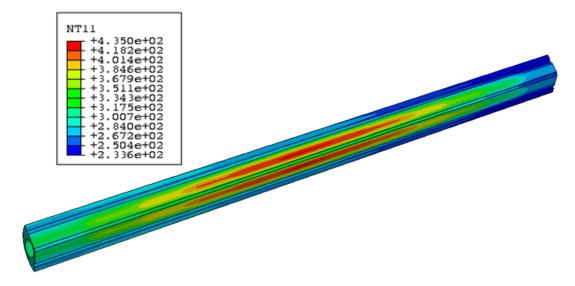


Figure 16. Axial temperature distribution (°F) in the hafnium aluminum absorber (base case).

Figure 17 shows the temperature distribution in the oxide layers at the coolant-heat sink interface. In this cutaway view, the oxide layers adjacent to the annulus, the center channel, and two off-center water channels are shown. The maximum oxide temperature (156°C, 312.8 °F) occurs below the core mid-plane in the oxide layer adjacent to the center water channel.

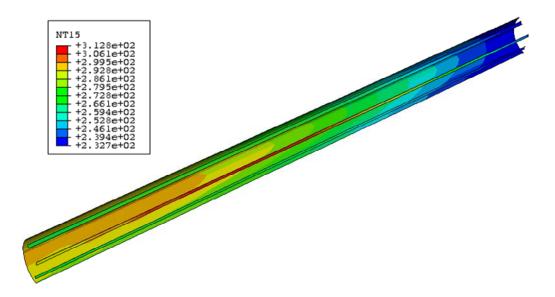


Figure 17. Temperature distribution (°F) in the oxide layers (base case).

Figure 18 shows the temperature distribution in the water coolant (a 120 degree sector of the model is displayed). The model is oriented with the water flowing from right to left. The maximum water channel temperatures are listed in Table 3. The temperature rise in the coolant is 32.7°C (58.8 °F) for the annulus, 25.6°C (46.1 °F) for the center water channel, and 14.9°C (26.8°F) in the off-center water channels. At a coolant pressure of 12.4 MPa (1800 psia), the saturation temperature for water is 323 °C (614 °F).

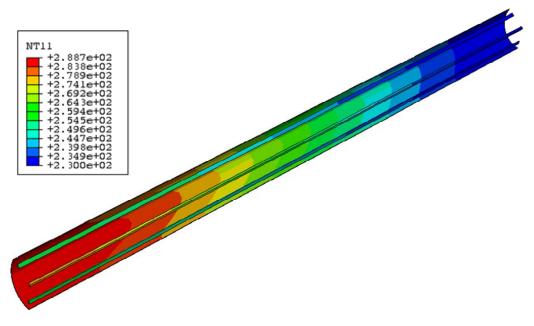


Figure 18. Temperature distribution (°F) in the water coolant (base case).

Table 3. Computed water channel outlet temperatures.

Location	T _{max} (°C / °F)
Water annulus	142.7 / 288.8
Center water channel	135.6 / 276.1
Three off-center water channels	124.9 / 256.8

Figures 19 and 20 show the heat flux distributions at the pressure tube and oxide surfaces. The magnitude of heat flux is negative for the pressure tube since heat flows out of this component. The maximum oxide layer heat flux occurs at core mid-plane and is the highest in the oxide layer adjacent to the center water channel. The maximum surface heat fluxes are given in Table 4.

Table 4. Computed maximum surface heat flux.

Location	q _{max} " (W/cm ² / BTU/s-in ²)
Oxide surface contacting water annulus	77.04 / 0.4714
Oxide surface contacting center water channel	291.1 / 1.781
Oxide surface contacting off-center water channels	221.0 / 1.352
Pressure tube surface contacting water annulus	-22.88 / -0.1406

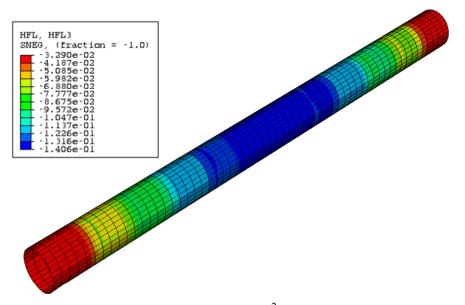


Figure 19. Distribution of surface heat flux (BTU/s-in²) at the pressure tube (base case).

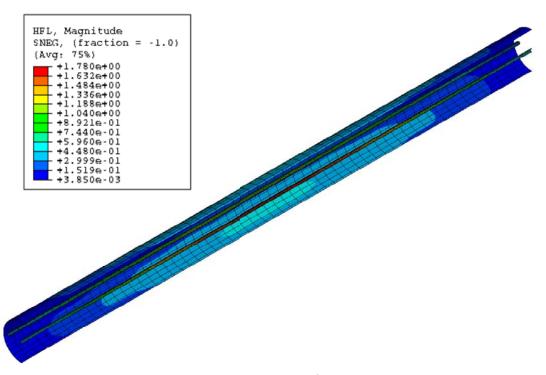


Figure 20. Distribution of surface heat flux (BTU/s-in²) at the oxide surfaces (base case).

The calculated flow instability ratio (FIR) and departure from nucleate boiling ratio (DNBR) for this configuration under nominal conditions are 6.5 and 8.0, respectively. These FIR and DNBR estimates are scoping calculations to show design feasibility under nominal conditions. Once the design is finalized, the FIR and DNBR should be evaluated at pump coast-down conditions with a safety factor on reactor power.

For the alternate configuration, with the added heat flux coming from the experiment chambers, temperatures were expectedly higher. Tables 5 and 6 list the outlet water temperature and the maximum surface heat flux for this configuration. Graphical depictions of these temperature distributions are provided in Appendix B.

Table 5. Computed water channel outlet temperatures for the alternate (added heat flux) configuration.

Location	T _{max} (°C / °F)
Water annulus	158.3 / 316.9
Center water channel	153.4 / 308.1
Three off-center water channels	133.4/ 272.1

Table 6. Computed maximum surface heat flux for the alternate (added heat flux) configuration.

Location	q _{max} " (W/cm² / BTU/s-in²)
Oxide surface contacting water annulus	134.1 / 0.8219
Oxide surface contacting center water channel	510.2 / 3.120
Oxide surface contacting off-center water channels	379.9 / 2.323

3.1.2.3 Conclusions from Thermal Analysis

The design of the water coolant and hafnium aluminum absorber presented here is capable of maintaining all system components below their maximum temperature limits. The maximum temperature of this conduction cooling system, 224.2°C (435.6 °F) occurs in a small, localized region in the heat sink structure near the core mid-plane. The calculated Flow Instability Ratio and Departure from Nucleate Boiling Ratio for this configuration under nominal conditions are 6.5 and 8.0, respectively, which safely exceed the minimum values of 2.0. For the alternate (added heating) configuration, the maximum temperature of the cooling system was 306.4°C (583.5 °F) in the same location. Either of these temperatures is well below the melting temperature of the aluminum (660°C). The total coolant flow rate requirement for this configuration is 207 L/min (54.7 gpm). The design can be further optimized to reduce the amount of pressurized water coolant. Achieving a minimum total volume of water coolant is desirable from a neutronics standpoint since water is a neutron moderator and will thermalize the neutrons.

3.2 Materials Issues

The use of hafnium to harden the neutron spectrum for the Gas Test Loop presented some design challenges to provide cooling. Solid hafnium produces a great deal of heat density and appeared to be difficult to cool with the gas coolant previously designed into the GTL. The alternative presented here uses solid aluminum as a cooling medium (the Al itself is water cooled) with the hafnium (Hf) dispersed throughout the aluminum. The use of this combination of materials presents several issues that should be discussed.

- Can the Hf be encased in Al in a stable form?
- What should be the Hf content?
- What should be the Hf distribution (particle size and distribution)?
- Can a machinable block of the composite material be fabricated?
- Can the block be machined or fabricated with coolant channels?
- What are the thermal/mechanical properties of the component materials?
- Will the composite be susceptible to corrosion as water passes through it.

Answers to these questions are now discussed.

3.2.1 Can the Hf be encased in Al in a stable form?

The goal is to make a dispersion/solution of Hf in Al. The options appear to be (1) mixed powders of Hf and Al, pressed together and machined or extruded,(2) a 2-phase aluminide and aluminum single block created by similarly mixing powders (Al and aluminide) or by melt alloying Hf with Al, followed by a subsequent heat treatment, or (3) mixed powders of HfO₂ and Al, pressed and machined or extruded.

The potential problems are (1) fabricability, (2) phase stability during fabrication and irradiation, (3) thermal conductivity of the various phases, and material property stability in reactor. Fabricability issues include creating composite material shapes with long, narrow flow channels and stability of aluminide phases or of HfO₂ compared to the Al matrix (this is also an operational issue), .

Hf-Al Mixtures:

The binary phase diagram (see Figure 21 below [10]) indicates that there is very little or no solubility of Hf in Al; intermetallics form across nearly the entire binary diagram. Knowing there will be free aluminum (excess Al) in the composite, the important intermetallic phase is that containing the least amount of Hf, namely Al₃Hf. The phase diagram indicates that a 5-10 at.% Hf mixture should consist of Al₃Hf in Al, the Al₃Hf being stable. The only question is whether in the as-fabricated state there are metastable conditions to be addressed.

Other things that the phase diagram indicate include that this mixture of Al₃Hf and Al is stable up to the melting temperature of Al, so the limiting condition is to maintain operating temperatures below the melting temperature of Al, a condition that is required by ATR anyway. Also, the phase diagram indicates that a mixture of Hf and Al would not be stable, that the intermetallic would form anyway, perhaps in a series of intermetallics. In addition, the intermetallic formation results in Al₃Hf with a density of 6.4 g/cm3 as calculated from the single crystal volume [11] and number of Hf and Al atoms in a unit cell, 12 and 4 [12], respectively. By rule of mixtures the density should be 5.3 g/cm3, so the mixture of materials increases in density as it forms the intermetallic, and thus would create voids/defects in the material as it precipitates.

These factors suggest that:

- 1. Al₃Hf is stable in an Al matrix.
- 2. The Al and Al₃Hf composite should not be created by mixing Hf and Al powders and reacting in the bulk because defects would form.

HfO₂ in Aluminum:

Another potential composite material that could be used as the neutron flux hardener could be HfO₂ in Al. The HfO₂ is dense/heavy (9.7 g/cm³) compared to Al (Note that Al has a density of 2.7 g/cm³, Hf is 13.1 g/cm³, and Al₃Hf is 6.4 g/cm³). A large difference in density can be a challenge in mixing the powders for pressing compacts, and maintaining a uniform dispersion. This could dictate a small range of usable oxide particle sizes.

Another potentially more serious problem is whether the HfO₂ is stable compared to Al₂O₃. This issue has arisen previously when uranium oxide and neptunium oxide were studied for use in an

aluminum matrix, as a fuel and as a target to form Pu-238, respectively. All three elements, Hf, Np, and U, are included in Figure 22 below, the diagram indicating the relative stability of

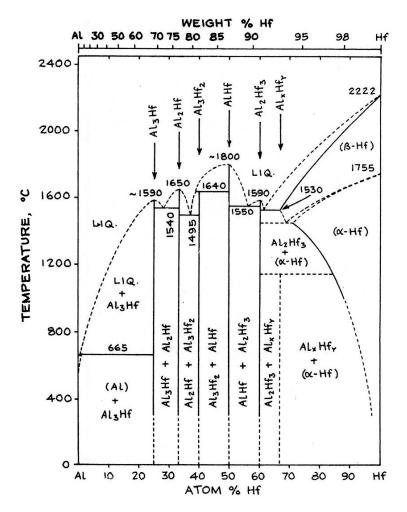


Figure 21. Aluminum-Hafnium Phase Diagram.

the oxides. NpO₂ appears to be the least stable. In fact, NpO₂ reduction problems during fabrication of NpO₂/Al targets were observed.[13]

In addition, uranium oxide in aluminum has long been used as a fuel type (for example, in HFIR). Early in the development of a fuel, ORNL workers [14] noted that Al would reduce UO_2 at $600^{\circ}C$ and form UAl_4 . A net volume increase, as much as 20-30%, accompanied the reaction. They subsequently used U_3O_8 in Al as fuel [15], the U_3O_8 being a more stable oxide. These experiences, with Np and U, suggest that there may also be problems with the stability of HfO_2 in Al.

Conclusions

The recommended composite material is Al₃Hf in an Al matrix. This has a good chance of being very stable and may also be fabricable, using a mixture of Al₃Hf and Al powders, compacting and hot pressing, or extruding.

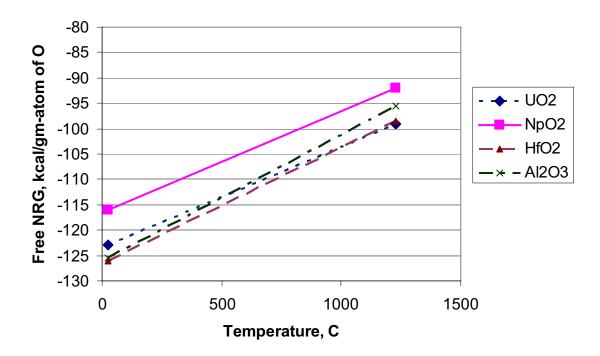


Figure 22. Free energy of formation of aluminum, uranium, neptunium, and hafnium oxides as a function of temperature.

3.2.2 What should be the Hf (Al₃Hf) content?

Recall from the "Physics" section of this report that the optimum Hf content is ~ 7 at. %. Assuming this atomic fraction is represented in the form of Al₃Hf in Al, the volume percentage of Al₃Hf required is about 23 %.

3.2.3 What should be the Hf distribution (particle size and distribution)?

From a fabricability standpoint, namely to achieve a successful and relatively stable mixture of Al₃Hf and Al powders, the relative sizes of the particles requires consideration. The Al₃Hf material is more than twice as dense as the Al, so un-mixing can be a problem. Mitigation may require equal sized powders, or much larger Al₃Hf powders. The theory behind the latter is that the large Al₃Hf particles need to displace a great many Al particles in order to un-mix the mixed powders; there remains a driving force for un-mixing but the process is more difficult and the unmixing rate is slowed.

3.2.4 Can a machinable block of the composite material be fabricated and /or can the block be machined or fabricated with coolant channels?

There are several potential methods of fabricating the 7 cm (2.8-inch) diameter cylinder of the composite and assembling one piece or several joined pieces into a four-foot length, complete with a number of small flow channels, and three larger channels to hold the test fuel samples. Ideas included:

- 1. Pressing composites of that diameter in short lengths, machining to size, drilling, and welding the pieces together. Problems include ensuring that the flow channels have no leaks, and welding with the composites.
- 2. Extruding a solid cylinder of the composite and then machining the coolant and sample channels, as well as the outer dimension. The obvious challenge is to machine the flow channels over the distance required.
- 3. Extruding the cylinder with the flow channels in-place, resulting from a complex extrusion. Machine the outer dimensions if required. The challenge results from the fact complex extrusions like this require points where the billet is split and reformed together through pressure welding. This is often done with aluminum extrusions, but the effects of the presence of the intermetallic on the welding process, and vice versa, are unknown. This, however, appears the most promising method.

Of course a simpler extrusion can be used if the cylinder is made of three sections (an alternate design), with the coolant water flowing between the flats of the sections. Machining can be used to finish the sections. The final extrusion process can be prescribed when the design is set.

It should be pointed out here that there is a precedent for machining long cooling channel flow channels. The beryllium reflector blocks that surround the ATR fuel have such holes machined in them. These blocks are the full (1.2-m) core height and the holes are drilled all the way through. The company that does this machining for the ATR blocks has indicated that some investigation would be needed on this different material to find the best way to drill such holes in the hafnium-aluminum.[16]

3.2.5 What are the thermal/mechanical properties of the component materials?

The matrix material is aluminum and certainly all of its relevant properties are known, including any effects of irradiation on the properties. The intermetallic, Al₃Hf is another matter. There is some thermodynamic information concerning enthalpy changes during decomposition and vapor pressure [17], but very little else is available concerning other properties.

Thermal Conductivity

The thermal conductivity has apparently not been measured. Al₃Hf does, however, possess the same crystal structure as Al₃Zr, tetragonal, D0₂₃ [11, 18]. At temperatures greater than 650°C Al₃Hf transforms to D0₂₂ [11], also tetragonal but with less tetragonality (a~c). The material should not be operating above 650°C without perhaps encroaching on the melting temperature of the aluminum matrix. It has been assumed for this assessment that the structure is D0₂₃. The thermal conductivity of Al₃Zr was measured at room temperature [19]. The value was found to be 42 W/m/°K (24.3 Btu/h/ft/°F).

The thermal conductivity of the composite material (Al with Al₃Hf) may also be important. The thermal conductivity of a composite with uranium and uranium aluminide (UAl₄) has been measured [20]. As with Hf in Al, U in Al has no solubility at temperatures less than 640 °C so it may be assumed, by inspection of the phase diagram, the samples were mixtures of 'pure' uranium and a UAl₄ intermetallic. The thermal conductivities shown below in Figure 23 were measured at 338 °K (65 °C). The maximum U content in the samples was 7.7 at. %; with U in UAl₄ being 20 at. %, ideally 38.7 % of the phase mixture would be the intermetallic phase.

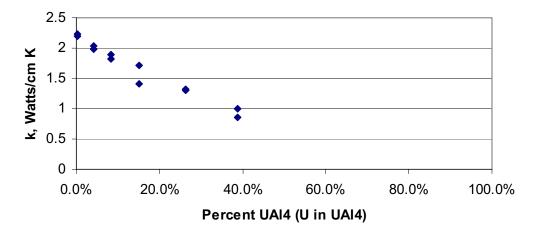


Figure 23. Measured Thermal Conductivity of Al-Al₄U Composite Material. The percentage of Al₄U is presented in at.%, or vol. % if the density can be approximated by rule of mixtures of the two elements, U and Al.

The dependency of thermal conductivity on the phase mixture shown below has been shown to fit a model, and this same model could be used to estimate the thermal conductivity of the Al-Al₃Hf composite. If the thermal conductivity of Al₃Hf is nearly the same as the conductivity of Al₃Zr then one would expect the 23% (by volume) Al₃Hf composite to have a thermal conductivity a little more than half that of pure Al.

Note that pure Hf has a thermal conductivity of 0.22 W/cm ° K @338 °K.

Samples of Al_3Hf have been produced for this project and thermal conductivities will be measured at temperatures between room temperature and $600^{\circ}C$. Having that knowledge, we can model the composite and predict the conductivity as a function of temperature.

Mechanical Properties

Intermetallic phases are usually very brittle materials. Examining specific intermetallics, it is known that those with more symmetric crystal structures (for example, cubic structures) and those with smaller lattice parameters are more ductile [21]. In this case the $D0_{23}$ structure has reasonable symmetry, but it is not as likely to have the ductility of the higher temperature phase, $D0_{22}$, as the crystal structure is very nearly cubic (a~c). The consequence of having a brittle intermetallic phase may be that the particles break as the composite is extruded, and it may be difficult to pressure bond to the surface of an Al_3Hf particle. Break-up of particles should be no problem, and the 'pressure welding' can be tested.

Effects of Irradiation

The radiation effects that are commonly associated with intermetallic phases are amorphization and phase stability (increased or decreased). While Zr₃Al has been irradiated in a number of studies, and found to be very sensitive to amorphization [22, 23], its structure is not the same as Al₃Zr, or Al₃Hf. There does not seem to be a great deal of information concerning intermetallics with structural similarity to Al₃Hf. Amorphization would not seem to be a particular problem for this application, although it could affect physical properties such as thermal conductivity. Resolution of the phase into the aluminum matrix would also not seem to be a problem.

To help resolve this uncertainty, small coupons of the Hf-Al material will be included in booster fuel mini-plate testing being conducted for the GTL/BFFL. In those tests, small samples 2.54 cm (1 inch) wide, 2.54 mm (0.100 inch) thick and of lengths up to 10.16 cm (4 inches) of one or more Hf-Al compositions will be included in capsules containing samples of the GTL/BFFL booster fuel material, irradiated for approximately 60 days, and examined for material changes.

3.2.6 Will the composite be susceptible to corrosion as water passes through it?

The water in the coolant loop should operate well below 300°C; the saturation temperature for 12.4-MPa (1800-psi) water is slightly greater than 300°C. Moreover, boehmite, or diaspore (high pressure/temperature phase) layers are not effective corrosion protection at temperatures greater than 300°C. We will assume that pure or low-alloy aluminum can be used exposed to the coolant channel water. Samples of the hafnium aluminum material will be included in mini-plate irradiation tests currently planned to examine booster fuel corrosion.

Another issue is the potential that the Al-Al₃Hf interface could create electric potentials or stresses from thermal expansion mismatch that would encourage corrosion at the interface. The particles could be loosened from the matrix and lost to the water. Also, the particles of aluminide themselves may not be corrosion resistant.

While the loss of small amounts of Hf to the water would be unacceptable if lost to the reactor coolant, the water that the material is exposed to in this case is contained within a loop. Nonetheless, it would be prudent to mitigate any corrosion, especially if corrosion is so severe to put the flow channels in jeopardy.

Assuming the Al-Al₃Hf material alone is expected to corrode at an unacceptable rate, mitigating steps could take the form of lining the coolant channels – another fabrication challenge. Another design, where the center block is fabricated in three pieces, and the water flows between the flats mating each of the three segments, may be amenable to cladding, but for this report we assume that the coolant flows through cylindrical channels in the composite block.

Another suggestion intended to avoid corrosion issues was to use zirconium and to incorporate hafnium in solution. The problem with this is the relatively low thermal conductivity of Zr compared to Al and its alloys (see Table 7 below). All of the aluminum-based materials, including the alloys, have much better thermal conductivity than Zr or Hf.

Table 7. Thermal	Conductivity of	Candidate Materials for	Thermal Neutron Absorber

Material	Thermal Conductivity, W/m°K,	Thermal Conductivity, W/m°K,
	@ 25 °C	@ 300 °C
Al [24]	250	200
Zr [25]	21	19
Hf [26]	22	21
6063 AI [27]	200	200
5456-H343 AI [28]	110	130

It will be assumed for the present that un-coated/clad Al-Al₃Hf will be used and will provide sufficient corrosion resistance. An extrusion process will be used to fabricate the design, either a simple extrusion, one in which pressure welding as part of a more complex extrusion process. The method will be prescribed dependent on the final design characteristics (cylinder with flow channels or three-section cylinder) of the body. To help ensure acceptable corrosion properties, the material will be irradiation tested, as indicated in the previous section, and corrosion will be examined in the post irradiation examination. Further corrosion issues can be investigated by proof testing when the design is more mature and mitigating features added if required.

It should be observed also that because of Hf burn-out, the hafnium-aluminum absorber will require replacement at regular intervals to maintain the thermal neutron absorber efficiency required for testing. Exact replacement frequency will be determined by the final design and by utilization and reactor operating history, but it may be as often as every 3 or 4 reactor operating cycles. Hence, the resistance to corrosion need not be perfect, so long as no significant performance changes take place during the absorber lifetime. Let it also be observed that the transmutation product of Hf, after multiple stages of neutron absorption in Hf, is mainly Ta-181, which is stable, and that corrosion would mainly impact thermal hydraulic performance, not primary coolant contamination with fission products.

4.0 IMPLEMENTATION

Besides the issues associated with functional performance of the BFFL as an entity in the reactor, there are a number of interfaces with the reactor and other systems at ATR that require resolution before the concept can be declared a success. Some of these remained issues for the earlier GTL configuration.

4.1 Secondary Coolant System

A key assumption to this point has been the availability of a secondary coolant system that sustains nominally 12.4 MPa (1,800 psi) water flows at flow rates adequate to achieve the required cooling. Several options exist for supplying that coolant.

First, a potential installation location for the BFFL in the ATR is the NW lobe. The experiment presently occupying that lobe makes use of a pressurized water secondary coolant system that is already installed and that would be fully capable of providing the required cooling with a 681 L/min (180 gpm) flow capability. That system is owned by the Naval Reactors Program. If it is left in place and available when the existing in-pile hardware is removed, it would provide the most cost-effective supply of pressurized secondary coolant.

If that is not feasible or if we use the NE Lobe instead, another pressurized water system, the one in the 2A cubicle, is being restored to service as part of the operating contract agreement between DOE and Battelle Energy Alliance. That restoration is planned for completion about the same time as the BFFL will be coming on line. At the present time, no other programs that would make use of this pressurized cooling system have been identified, and it should be available for use, should it be needed. Running the coolant lines from the reactor vessel penetration to the BFFL experiment and back would be the responsibility of the BFFL project. The available flow rate for this system is 227 L/min (60 gpm).

A third pressurized cooling system exists in the 1D cubicle. Its available flow rate is only 151 L/min (40 gpm), but is also capable of pressures in excess of 12.4 MPa (1,800 psig).

4.2 Temperature Control Gas System

As with the GTL, the BFFL will make use of a mixed-gas experiment temperature control system. This technique has been used for many years as a means of controlling temperatures in lead-type experiments. Using this approach, a narrow gas gap is installed between the experiment capsule and the cooling medium for removing heat from the experiment. This gap is filled with a mixture of helium and a heavy gas such as neon or argon. When pure helium is present, the thermal conductivity of the gas in the gap is much greater than when the heavier gas is present. Temperature feedback to the gas mixing system provides the ability to adjust the mixture and thus achieve control of the experiment temperature, even when heating rates vary because of reactor power variations or other factors.

The number of channels of temperature control needed remains to be fixed by BFFL design, but the GTL conceptual design had as many as 15, five in each of the three irradiation columns. In this aspect it was similar to the Irradiation Test Vehicle (ITV), which had been installed in the center flux trap but has recently been removed. With the ITV, as will doubtless be the case with BFFL, the specific implementation of temperature control was unique to the individual experiments.[6] The temperature control gas system was then set up to meet the needs of the individual experiments. The temperature control gas system from the ITV has been removed, but it could be restored and adapted for use on BFFL. If that proves infeasible, there are other projects making use of such systems. The engineering of these systems has been completed, and it would be straightforward to adapt the design to the needs of the BFFL.

4.3 System Interfaces

A non-trivial engineering challenge remaining to be worked through in the BFFL concept is the interfacing of the secondary cooling system with the temperature control gas system. Both of these will be interior to the ASME Section III pressure boundary between the BFFL experiment and the ATR Primary Cooling System. Existing experiments using pressurized secondary cooling systems have engineered solutions to the need for inserting experiments inside the pressure tube interface. It is expected that those same solutions will be applicable to BFFL. The resolving of these engineering issues is not part of the scope of this feasibility study.

5.0 COST IMPACT

The primary objective in undertaking this investigation was to seek a technically viable configuration that would result in overall savings in system cost. A detailed cost estimate had

been prepared for the prior GTL configuration that resulted in a total project cost rounded to \$84M. Uncertainties and project delays since that estimate led to a more practical cost range of \$80-100M.

The detailed GTL cost estimate was the point of departure for preparing a revised estimate for the BFFL total system cost. Many elements of the earlier estimate were carried forward unchanged, for example the cost of developing the booster fuel used in both configurations. Some elements in the earlier estimate, such as the pressurized gas cooling system, did not appear at all in the new estimate. Other costs, such as connecting to the pressurized water loop were new in the BFFL estimate, not appearing in the earlier GTL estimate. One other category of costs shown in both estimates, although it may not really be required, is the cost of neutrons for irradiation testing of booster fuel plates and the complete BFFL system in the ATR prior to considering it a completed project. It is not known at this time whether such irradiation charges will be incurred by the project, but they probably will appear somewhere, at some level, in overall system acquisition, so they were included in the estimate.

The total project cost summary report is provided in Appendix C. The bottom line comparison of the BFFL cost with the GTL cost shows a reduction of approximately \$25-30M by changing to the BFFL configuration. Even with irradiation charges for single plate irradiation and first-operation demonstration tests of more than \$11M included, the project cost is now estimated at between \$50M and \$75M. The estimated cost with a 25% contingency was \$63.4M. The \$50M figure is a nominal cost without contingency and the higher \$75M figure is with about 50% contingency, which would not be unreasonable for this stage of concept development. Hence, this investigation has shown that a technically viable alternatively cooled configuration can be produced that results in substantial total cost savings over the original GTL design.

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APPENDIX A DETAILED CALCULATIONS USED IN THERMAL ANALYSIS

Table A-1. Material Properties used in analysis.

1 00010			Р		<i>y</i>		
Inconel-6		1 (141/ 17)	I (D) (: 0E)				
T(°C)	T(°F) 302		k (Btu/s-in-°F)				
150 300		14.8 17.5	1.979E-04 2.341E-04				
450		20.2	2.702E-04				
600		23.9	3.197E-04				
000	, 1112	20.0	3.137 L-04				
density							
(kg/m3)	(lbm/in3)						
8470	,						
0470	0.500						
specific he	eat						
(J/kg-K)	(Btu/lbm-°F)						
444	,						
Al-Hf Allo	У						
T(°C)	T(°F)	k (W/m-K)	k (Btu/s-in-°F)				
		213.8	2.860E-03				
density							
(kg/m3)	(lbm/in3)						
3440	0.124						
specific he							
(J/kg-K)	(Btu/lbm-°F)						
	0.223						
Oxide	W. (O.E.)	1 000	1 (D) () ==				
T(°C)	T(°F)	, ,	k (Btu/s-in-°F)				
		2.25	3.009E-05				
density							
(kg/m3)	(lbm/in3)						
	0.0975						
	-4						
specific he							
(J/kg-K)	(Btu/lbm-°F)						
	0.212						
Halium					t=0.02 inch gan	t=0.04 inch gan	
	T(°C)	T(°E)	k (\M/m K)	k (Btu/s in °E)	t=0.02 inch gap		
T(K)	T(°C)	T(°F)	, ,		h (Btu/s-in ² -°F)	h (Btu/s-in²-°F)	
T(K) 373.1	100.1	212.18	0.1753	2.345E-06	h (Btu/s-in ² -°F) 1.173E-04	h (Btu/s-in ² -°F) 5.863E-05	
T(K) 373.1 473.1	100.1 200.1	212.18 392.18	0.1753 0.2092	2.345E-06 2.798E-06	h (Btu/s-in ² -°F) 1.173E-04 1.399E-04	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05	
T(K) 373.1 473.1 573.1	100.1 200.1 300.1	212.18 392.18 572.18	0.1753 0.2092 0.2301	2.345E-06 2.798E-06 3.078E-06	h (Btu/s-in ² -°F) 1.173E-04 1.399E-04 1.539E-04	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05	
T(K) 373.1 473.1 573.1 673.1	100.1 200.1 300.1 400.1	212.18 392.18 572.18 752.18	0.1753 0.2092 0.2301 0.2569	2.345E-06 2.798E-06 3.078E-06 3.437E-06	h (Btu/s-in ² -°F) 1.173E-04 1.399E-04 1.539E-04 1.718E-04	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05 8.591E-05	
T(K) 373.1 473.1 573.1 673.1 773.1	100.1 200.1 300.1 400.1 500.1	212.18 392.18 572.18 752.18 932.18	0.1753 0.2092 0.2301 0.2569 0.2895	2.345E-06 2.798E-06 3.078E-06 3.437E-06 3.873E-06	h (Btu/s-in ² -°F) 1.173E-04 1.399E-04 1.539E-04 1.718E-04 1.936E-04	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05 8.591E-05 9.682E-05	
T(K) 373.1 473.1 573.1 673.1 773.1 873.1	100.1 200.1 300.1 400.1 500.1 600.1	212.18 392.18 572.18 752.18 932.18 1112.18	0.1753 0.2092 0.2301 0.2569 0.2895 0.3171	2.345E-06 2.798E-06 3.078E-06 3.437E-06 3.873E-06 4.242E-06	h (Btu/s-in ² -°F) 1.173E-04 1.399E-04 1.539E-04 1.718E-04 1.936E-04 2.121E-04	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05 8.591E-05 9.682E-05 1.060E-04	
T(K) 373.1 473.1 573.1 673.1 773.1 873.1 973.1	100.1 200.1 300.1 400.1 500.1 600.1 700.1	212.18 392.18 572.18 752.18 932.18 1112.18 1292.18	0.1753 0.2092 0.2301 0.2569 0.2895 0.3171 0.3422	2.345E-06 2.798E-06 3.078E-06 3.437E-06 3.873E-06 4.242E-06 4.578E-06	h (Btu/s-in ² -°F) 1.173E-04 1.399E-04 1.539E-04 1.718E-04 1.936E-04 2.121E-04 2.289E-04	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05 8.591E-05 9.682E-05 1.060E-04 1.144E-04	
T(K) 373.1 473.1 573.1 673.1 773.1 873.1 973.1	100.1 200.1 300.1 400.1 500.1 600.1 700.1 800.1	212.18 392.18 572.18 752.18 932.18 1112.18 1292.18 1472.18	0.1753 0.2092 0.2301 0.2569 0.2895 0.3171 0.3422 0.3661	2.345E-06 2.798E-06 3.078E-06 3.437E-06 3.873E-06 4.242E-06 4.578E-06 4.897E-06	h (Btu/s-in ² -°F) 1.173E-04 1.399E-04 1.539E-04 1.718E-04 1.936E-04 2.121E-04 2.289E-04 2.449E-04	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05 8.591E-05 9.682E-05 1.060E-04 1.144E-04	
T(K) 373.1 473.1 573.1 673.1 773.1 873.1 973.1 1073.1	100.1 200.1 300.1 400.1 500.1 600.1 700.1 800.1 900.1	212.18 392.18 572.18 752.18 932.18 1112.18 1292.18 1472.18 1652.18	0.1753 0.2092 0.2301 0.2569 0.2895 0.3171 0.3422 0.3661 0.4004	2.345E-06 2.798E-06 3.078E-06 3.437E-06 3.873E-06 4.242E-06 4.578E-06 4.897E-06 5.356E-06	h (Btu/s-in ² -°F) 1.173E-04 1.399E-04 1.539E-04 1.718E-04 1.936E-04 2.121E-04 2.289E-04 2.678E-04	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05 8.591E-05 9.682E-05 1.060E-04 1.144E-04 1.224E-04	
T(K) 373.1 473.1 573.1 673.1 773.1 873.1 973.1 1073.1 1173.1	100.1 200.1 300.1 400.1 500.1 700.1 800.1 900.1	212.18 392.18 572.18 752.18 932.18 1112.18 1292.18 1472.18 1652.18 1832.18	0.1753 0.2092 0.2301 0.2569 0.2895 0.3171 0.3422 0.3661 0.4004 0.4226	2.345E-06 2.798E-06 3.078E-06 3.437E-06 4.242E-06 4.578E-06 4.897E-06 5.356E-06 5.653E-06	h (Btu/s-in ² -°F) 1.173E-04 1.399E-04 1.539E-04 1.718E-04 1.936E-04 2.121E-04 2.289E-04 2.449E-04 2.678E-04 2.827E-04	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05 8.591E-05 9.682E-05 1.060E-04 1.144E-04 1.224E-04 1.339E-04	
T(K) 373.1 473.1 573.1 673.1 773.1 873.1 973.1 1073.1	100.1 200.1 300.1 400.1 500.1 700.1 800.1 900.1	212.18 392.18 572.18 752.18 932.18 1112.18 1292.18 1472.18 1652.18	0.1753 0.2092 0.2301 0.2569 0.2895 0.3171 0.3422 0.3661 0.4004	2.345E-06 2.798E-06 3.078E-06 3.437E-06 3.873E-06 4.242E-06 4.578E-06 4.897E-06 5.356E-06	h (Btu/s-in ² -°F) 1.173E-04 1.399E-04 1.539E-04 1.718E-04 1.936E-04 2.121E-04 2.289E-04 2.449E-04 2.678E-04 2.827E-04	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05 8.591E-05 9.682E-05 1.060E-04 1.144E-04 1.224E-04	
T(K) 373.1 473.1 573.1 673.1 773.1 873.1 973.1 1073.1 1173.1 1273.1	100.1 200.1 300.1 400.1 500.1 700.1 800.1 900.1	212.18 392.18 572.18 752.18 932.18 1112.18 1292.18 1472.18 1652.18 1832.18	0.1753 0.2092 0.2301 0.2569 0.2895 0.3171 0.3422 0.3661 0.4004 0.4226	2.345E-06 2.798E-06 3.078E-06 3.437E-06 4.242E-06 4.578E-06 4.897E-06 5.356E-06 5.653E-06	h (Btu/s-in ² -°F) 1.173E-04 1.399E-04 1.539E-04 1.718E-04 1.936E-04 2.121E-04 2.289E-04 2.449E-04 2.678E-04 2.827E-04	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05 8.591E-05 9.682E-05 1.060E-04 1.144E-04 1.224E-04 1.339E-04	
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T(K) 373.1 473.1 573.1 673.1 773.1 873.1 1073.1 1173.1 1273.1 1333.1 density (kg/m3) 0.1787	100.1 200.1 300.1 400.1 500.1 600.1 700.1 800.1 900.1 1000.1 1060.1	212.18 392.18 572.18 752.18 932.18 1112.18 1292.18 1472.18 1652.18 1832.18	0.1753 0.2092 0.2301 0.2569 0.2895 0.3171 0.3422 0.3661 0.4004 0.4226	2.345E-06 2.798E-06 3.078E-06 3.437E-06 4.242E-06 4.578E-06 4.897E-06 5.356E-06 5.653E-06	h (Btu/s-in ² -°F) 1.173E-04 1.399E-04 1.539E-04 1.718E-04 1.936E-04 2.121E-04 2.289E-04 2.449E-04 2.678E-04 2.827E-04	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05 8.591E-05 9.682E-05 1.060E-04 1.144E-04 1.224E-04 1.339E-04	
T(K) 373.1 473.1 573.1 673.1 773.1 873.1 1073.1 1173.1 1273.1 1273.1 density (kg/m3) 0.1787 specific he	100.1 200.1 300.1 400.1 500.1 600.1 700.1 800.1 900.1 1000.1 1060.1	212.18 392.18 572.18 752.18 932.18 1112.18 1292.18 1472.18 1652.18 1832.18	0.1753 0.2092 0.2301 0.2569 0.2895 0.3171 0.3422 0.3661 0.4004 0.4226	2.345E-06 2.798E-06 3.078E-06 3.437E-06 4.242E-06 4.578E-06 4.897E-06 5.356E-06 5.653E-06	h (Btu/s-in ² -°F) 1.173E-04 1.399E-04 1.539E-04 1.718E-04 1.936E-04 2.121E-04 2.289E-04 2.449E-04 2.678E-04 2.827E-04	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05 8.591E-05 9.682E-05 1.060E-04 1.144E-04 1.224E-04 1.339E-04	
T(K) 373.1 473.1 573.1 673.1 773.1 1073.1 1173.1 1273.1 1273.1 1333.1 density (kg/m3)	100.1 200.1 300.1 400.1 500.1 600.1 700.1 800.1 900.1 1000.1 1060.1	212.18 392.18 572.18 752.18 932.18 1112.18 1292.18 1472.18 1652.18 1832.18	0.1753 0.2092 0.2301 0.2569 0.2895 0.3171 0.3422 0.3661 0.4004 0.4226	2.345E-06 2.798E-06 3.078E-06 3.437E-06 4.242E-06 4.578E-06 4.897E-06 5.356E-06 5.653E-06	h (Btu/s-in ² -°F) 1.173E-04 1.399E-04 1.539E-04 1.718E-04 1.936E-04 2.121E-04 2.289E-04 2.449E-04 2.678E-04 2.827E-04	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05 8.591E-05 9.682E-05 1.060E-04 1.144E-04 1.224E-04 1.339E-04	
T(K) 373.1 473.1 573.1 673.1 773.1 873.1 1073.1 1173.1 1273.1 1333.1 density (kg/m3) 0.1787 specific he (J/kg-K)	100.1 200.1 300.1 400.1 500.1 600.1 700.1 800.1 900.1 1000.1 1060.1 (lbm/in3) 6.46E-06	212.18 392.18 572.18 752.18 932.18 1112.18 1292.18 1472.18 1652.18 1832.18	0.1753 0.2092 0.2301 0.2569 0.2895 0.3171 0.3422 0.3661 0.4004 0.4226	2.345E-06 2.798E-06 3.078E-06 3.437E-06 4.242E-06 4.578E-06 4.897E-06 5.356E-06 5.653E-06	h (Btu/s-in ² -°F) 1.173E-04 1.399E-04 1.539E-04 1.718E-04 1.936E-04 2.121E-04 2.289E-04 2.449E-04 2.678E-04 2.827E-04	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05 8.591E-05 9.682E-05 1.060E-04 1.144E-04 1.224E-04 1.339E-04	
T(K) 373.1 473.1 573.1 673.1 773.1 1073.1 1173.1 1273.1 1273.1 1333.1 density (kg/m3) 0.1787 specific he (J/kg-K) 5193	100.1 200.1 300.1 400.1 500.1 600.1 700.1 800.1 900.1 1000.1 1060.1 (lbm/in3) 6.46E-06	212.18 392.18 572.18 752.18 932.18 1112.18 1292.18 1472.18 1652.18 1832.18	0.1753 0.2092 0.2301 0.2569 0.2895 0.3171 0.3422 0.3661 0.4004 0.4226	2.345E-06 2.798E-06 3.078E-06 3.437E-06 4.242E-06 4.578E-06 4.897E-06 5.356E-06 5.653E-06	h (Btu/s-in ² -°F) 1.173E-04 1.399E-04 1.539E-04 1.718E-04 1.936E-04 2.121E-04 2.289E-04 2.449E-04 2.678E-04 2.827E-04	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05 8.591E-05 9.682E-05 1.060E-04 1.144E-04 1.224E-04 1.339E-04	
T(K) 373.1 473.1 573.1 673.1 773.1 873.1 1073.1 1173.1 1273.1 1273.1 1333.1 density (kg/m3) 0.1787 specific he (J/kg-K) 5193	100.1 200.1 300.1 400.1 500.1 600.1 700.1 800.1 900.1 1000.1 1060.1 (lbm/in3) 6.46E-06	212.18 392.18 572.18 752.18 932.18 1112.18 1292.18 1472.18 1652.18 1832.18	0.1753 0.2092 0.2301 0.2569 0.2895 0.3171 0.3422 0.3661 0.4004 0.4226	2.345E-06 2.798E-06 3.078E-06 3.437E-06 4.242E-06 4.578E-06 4.897E-06 5.356E-06 5.653E-06	h (Btu/s-in ² -°F) 1.173E-04 1.399E-04 1.539E-04 1.718E-04 1.936E-04 2.121E-04 2.289E-04 2.678E-04 2.827E-04 2.902E-04	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05 8.591E-05 9.682E-05 1.060E-04 1.144E-04 1.224E-04 1.339E-04	
T(K) 373.1 473.1 573.1 673.1 773.1 873.1 1073.1 1173.1 1273.1 1273.1 density (kg/m3) 0.1787 specific he (J/kg-K) 5193	100.1 200.1 300.1 400.1 500.1 600.1 700.1 1000.1 1000.1 1060.1 (lbm/in3) 6.46E-06 eat (Btu/lbm-°F)	212.18 392.18 572.18 932.18 1112.18 1292.18 1472.18 1652.18 1832.18	0.1753 0.2092 0.2301 0.2569 0.2895 0.3171 0.3422 0.3661 0.4004 0.4226 0.4339	2.345E-06 2.798E-06 3.078E-06 3.437E-06 3.873E-06 4.242E-06 4.578E-06 5.356E-06 5.653E-06 5.804E-06	h (Btu/s-in ² -°F) 1.173E-04 1.399E-04 1.539E-04 1.718E-04 1.936E-04 2.121E-04 2.289E-04 2.678E-04 2.827E-04 2.902E-04	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05 8.591E-05 9.682E-05 1.060E-04 1.144E-04 1.224E-04 1.413E-04 1.451E-04	
T(K) 373.1 473.1 573.1 673.1 773.1 873.1 1073.1 1173.1 1273.1 1273.1 1333.1 density (kg/m3) 0.1787 specific he (J/kg-K) 5193	100.1 200.1 300.1 400.1 500.1 600.1 700.1 800.1 900.1 1000.1 1060.1 (lbm/in3) 6.46E-06 eat (Btu/lbm-°F) 3 1.24	212.18 392.18 572.18 932.18 1112.18 1292.18 1472.18 1652.18 1832.18 1940.18	0.1753 0.2092 0.2301 0.2569 0.2895 0.3171 0.3422 0.3661 0.4004 0.4226 0.4339	2.345E-06 2.798E-06 3.078E-06 3.437E-06 3.873E-06 4.242E-06 4.578E-06 5.356E-06 5.653E-06 5.804E-06	h (Btu/s-in ² -°F) 1.173E-04 1.399E-04 1.539E-04 1.718E-04 1.936E-04 2.121E-04 2.289E-04 2.678E-04 2.827E-04 2.902E-04	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05 8.591E-05 9.682E-05 1.060E-04 1.144E-04 1.339E-04 1.413E-04 1.451E-04	Density
T(K) 373.1 473.1 573.1 673.1 673.1 773.1 1073.1 1173.1 1273.1 1273.1 1333.1 density (kg/m3) 0.1787 specific he (J/kg-K) 5193 Water Tem (°F)	100.1 200.1 300.1 400.1 500.1 600.1 700.1 1000.1 1000.1 1060.1 (Ibm/in3) 6.46E-06 eat (Btu/lbm-°F) 3 1.24	212.18 392.18 572.18 752.18 932.18 1112.18 1292.18 1472.18 1652.18 1832.18 1940.18	0.1753 0.2092 0.2301 0.2569 0.2895 0.3171 0.3422 0.3661 0.4004 0.4226 0.4339	2.345E-06 2.798E-06 3.078E-06 3.437E-06 4.242E-06 4.578E-06 4.897E-06 5.356E-06 5.653E-06 5.804E-06	h (Btu/s-in²-°F) 1.173E-04 1.399E-04 1.539E-04 1.718E-04 1.936E-04 2.121E-04 2.289E-04 2.678E-04 2.827E-04 2.902E-04	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05 8.591E-05 9.682E-05 1.060E-04 1.144E-04 1.224E-04 1.339E-04 1.413E-04	Density (lbm/in3)
T(K) 373.1 473.1 673.1 673.1 673.1 1073.1 1173.1 1273.1 1273.1 1333.1 density (kg/m3) 0.1787 specific he (J/kg-K) 5193 Water Tem (°F) 300	100.1 200.1 300.1 400.1 500.1 600.1 700.1 800.1 900.1 1000.1 1060.1 (Ibm/in3) 6.46E-06 eat (Btu/lbm-°F) 3 1.24	212.18 392.18 572.18 932.18 1112.18 1292.18 1472.18 1652.18 1832.18 1940.18	0.1753 0.2092 0.2301 0.2569 0.2895 0.3171 0.3422 0.3661 0.4004 0.4226 0.4339	2.345E-06 2.798E-06 3.078E-06 3.437E-06 4.242E-06 4.578E-06 5.356E-06 5.653E-06 5.804E-06	h (Btu/s-in²-°F) 1.173E-04 1.399E-04 1.539E-04 1.718E-04 1.936E-04 2.121E-04 2.289E-04 2.678E-04 2.827E-04 2.902E-04	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05 8.591E-05 9.682E-05 1.060E-04 1.144E-04 1.339E-04 1.413E-04 1.451E-04	Density (lbm/in3) 0.036
T(K) 373.1 473.1 573.1 673.1 673.1 773.1 1073.1 1173.1 1273.1 1273.1 1333.1 density (kg/m3) 0.1787 specific he (J/kg-K) 5193 Water Tem (°F) 300 315	100.1 200.1 300.1 400.1 500.1 600.1 700.1 800.1 1000.1 1060.1 (Ibm/in3) 6.46E-06 eat (Btu/lbm-°F) 3 1.24	212.18 392.18 572.18 932.18 1112.18 1292.18 1472.18 1652.18 1832.18 1940.18	0.1753 0.2092 0.2301 0.2569 0.2895 0.3171 0.3422 0.3661 0.4004 0.4226 0.4339 k (Btu/s-in-°F) (Btu/s-in-°F) (Btu/s-in-°F) 8.20E-06 8.48E-06	2.345E-06 2.798E-06 3.078E-06 3.437E-06 4.242E-06 4.578E-06 5.356E-06 5.653E-06 5.804E-06	h (Btu/s-in²-°F) 1.173E-04 1.399E-04 1.539E-04 1.718E-04 1.936E-04 2.121E-04 2.289E-04 2.678E-04 2.827E-04 2.902E-04	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05 8.591E-05 9.682E-05 1.060E-04 1.144E-04 1.224E-04 1.339E-04 1.413E-04 1.451E-04	Density (lbm/in3) 0.036 0.036
T(K) 373.1 473.1 573.1 673.1 773.1 873.1 1073.1 1173.1 1273.1 1333.1 density (kg/m3) 0.1787 specific he (J/kg-K) 5193 Water Tem (°F) 300 315 325	100.1 200.1 300.1 400.1 500.1 600.1 700.1 1000.1 1000.1 1060.1 (lbm/in3) 6.46E-06 eat (Btu/lbm-°F) 3 1.24	212.18 392.18 572.18 932.18 1112.18 1292.18 1472.18 1652.18 1832.18 1940.18	0.1753 0.2092 0.2301 0.2569 0.2895 0.3171 0.3422 0.3661 0.4004 0.4226 0.4339 k (Btu/s-in-°F) (Btu/s-in-°F) 8.20E-06 8.48E-06 8.63E-06	2.345E-06 2.798E-06 3.078E-06 3.437E-06 3.873E-06 4.242E-06 4.578E-06 5.356E-06 5.653E-06 5.804E-06	h (Btu/s-in²-°F) 1.173E-04 1.399E-04 1.539E-04 1.718E-04 1.936E-04 2.121E-04 2.289E-04 2.289E-04 2.827E-04 2.902E-04	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05 8.591E-05 9.682E-05 1.060E-04 1.144E-04 1.224E-04 1.339E-04 1.413E-04 1.451E-04	Density (lbm/in3) 0.036 0.036
T(K) 373.1 473.1 673.1 673.1 673.1 1073.1 1173.1 1273.1 1273.1 1333.1 density (kg/m3) 0.1787 specific he (J/kg-K) 5193 Water Tem (°F) 300 315 325 325 335	100.1 200.1 300.1 400.1 500.1 600.1 700.1 1000.1 1000.1 1060.1 (Ibm/in3) 6.46E-06 eat (Btu/lbm-°F) 3 1.24	212.18 392.18 572.18 932.18 1112.18 1292.18 1472.18 1652.18 1832.18 1940.18 k (W/cm-°C) 6.13E-03 6.34E-03 6.45E-03	0.1753 0.2092 0.2301 0.2569 0.2895 0.3171 0.3422 0.3661 0.4004 0.4226 0.4339 k (Btu/s-in-°F) (Btu/s-in-°F) 8.20E-06 8.48E-06 8.63E-06 8.77E-06	2.345E-06 2.798E-06 3.078E-06 3.437E-06 4.242E-06 4.578E-06 5.356E-06 5.653E-06 5.804E-06	h (Btu/s-in²-°F) 1.173E-04 1.399E-04 1.539E-04 1.718E-04 1.936E-04 2.121E-04 2.289E-04 2.678E-04 2.827E-04 2.902E-04	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05 8.591E-05 9.682E-05 1.060E-04 1.144E-04 1.224E-04 1.339E-04 1.413E-04 1.451E-04	Density (lbm/in3) 0.036 0.036 0.036 0.035
T(K) 373.1 473.1 673.1 673.1 673.1 1073.1 1173.1 1273.1 1273.1 1333.1 density (kg/m3) 0.1787 specific he (J/kg-K) 5193 Water Tem (°F) 300 315 325 335 345	100.1 200.1 300.1 300.1 400.1 500.1 600.1 700.1 800.1 900.1 1000.1 1060.1 (lbm/in3) 6.46E-06 eat (Btu/lbm-°F) 3 1.24	212.18 392.18 572.18 932.18 1112.18 1292.18 1472.18 1652.18 1832.18 1940.18	0.1753 0.2092 0.2301 0.2569 0.2895 0.3171 0.3422 0.3661 0.4004 0.4226 0.4339 k (Btu/s-in-°F) 8.20E-06 8.48E-06 8.63E-06 8.77E-06 8.93E-06	2.345E-06 2.798E-06 3.078E-06 3.437E-06 4.242E-06 4.578E-06 5.356E-06 5.653E-06 5.804E-06	N (Btu/s-in²-°F) 1.173E-04 1.399E-04 1.539E-04 1.718E-04 1.936E-04 2.121E-04 2.289E-04 2.449E-04 2.827E-04 2.902E-04 Cp (Btu/lbm-°F) 0.998 0.998 0.999 1.000 1.001	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05 8.591E-05 9.682E-05 1.060E-04 1.144E-04 1.224E-04 1.339E-04 1.413E-04 1.451E-04	Density (lbm/in3) 0.036 0.036 0.036 0.035 0.035
T(K) 373.1 473.1 573.1 673.1 673.1 773.1 1073.1 1173.1 1273.1 1273.1 1333.1 density (kg/m3) 0.1787 specific he (J/kg-K) 5193 Water Tem (°F) 300 315 325 335 345 355	100.1 200.1 300.1 300.1 400.1 500.1 600.1 700.1 800.1 1000.1 1060.1 1060.1 (lbm/in3) 6.46E-06 eat (Btu/lbm-°F) 1.24	212.18 392.18 572.18 932.18 1112.18 1122.18 1472.18 1652.18 1832.18 1940.18	0.1753 0.2092 0.2301 0.2569 0.2895 0.3171 0.3422 0.3661 0.4004 0.4226 0.4339 k (Btu/s-in-°F) (Btu/s-in-°F) (Btu/s-in-°F) 8.20E-06 8.48E-06 8.63E-06 8.93E-06 8.97E-06	2.345E-06 2.798E-06 3.078E-06 3.437E-06 4.242E-06 4.578E-06 5.356E-06 5.653E-06 5.804E-06	Cp (Btu/lbm-°F) 0.998 0.998 0.999 1.000 1.001 1.001 1.001 1.001	Density (g/cm3) 0.997 0.991 0.987 0.971	Density (lbm/in3) 0.036 0.036 0.036 0.035 0.035
T(K) 373.1 473.1 573.1 673.1 773.1 873.1 1073.1 1173.1 1273.1 1333.1 density (kg/m3) 0.1787 specific he (J/kg-K) 5193 Water Tem (°F) 300 315 325 335 345 355 365	100.1 200.1 300.1 400.1 500.1 600.1 700.1 1000.1 1000.1 1000.1 1060.1 1060.1 (lbm/in3) 6.46E-06 eat (Btu/lbm-°F) 3 1.24	212.18 392.18 572.18 932.18 1112.18 1292.18 1472.18 1652.18 1832.18 1940.18	0.1753 0.2092 0.2301 0.2569 0.2895 0.3171 0.3422 0.3661 0.4004 0.4226 0.4339 k (Btu/s-in-°F) (Btu/s-in-°F) 8.20E-06 8.48E-06 8.63E-06 8.97E-06 9.06E-06	2.345E-06 2.798E-06 3.078E-06 3.437E-06 4.242E-06 4.578E-06 5.356E-06 5.653E-06 5.804E-06	h (Btu/s-in²-°F) 1.173E-04 1.399E-04 1.539E-04 1.539E-04 2.121E-04 2.289E-04 2.289E-04 2.827E-04 2.902E-04 2.902E-04 Cp (Btu/lbm-°F) 0.998 0.998 0.999 1.000 1.001 1.003	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05 8.591E-05 9.682E-05 1.060E-04 1.144E-04 1.224E-04 1.339E-04 1.413E-04 1.451E-04	Density (lbm/in3) 0.036 0.036 0.035 0.035 0.035
T(K) 373.1 473.1 673.1 673.1 673.1 1073.1 1173.1 1173.1 1273.1 1333.1 density (kg/m3) 0.1787 specific he (J/kg-K) 5193 Water Tem (°F) 300 315 325 335 345 355 345 355	100.1 200.1 300.1 400.1 500.1 600.1 700.1 800.1 900.1 1000.1 1060	212.18 392.18 572.18 932.18 1112.18 1292.18 1472.18 1652.18 1832.18 1940.18	k (Btu/s-in-°F) (Btu/s-in-°F) 8.20E-06 8.48E-06 8.63E-06 8.97E-06 9.06E-06 9.11E-06	2.345E-06 2.798E-06 3.078E-06 3.437E-06 3.873E-06 4.242E-06 4.897E-06 5.356E-06 5.653E-06 5.804E-06	Cp (Btu/lbm-°F) 0.998 0.999 1.000 1.001 1.003 1.005 1.005	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05 8.591E-05 9.682E-05 1.060E-04 1.144E-04 1.224E-04 1.339E-04 1.413E-04 1.451E-04 Density (g/cm3) 0.997 0.991 0.987 0.982 0.977 0.971 0.963 0.957	Density (lbm/in3) 0.036 0.035 0.035 0.035 0.035 0.035
T(K) 373.1 473.1 573.1 673.1 673.1 1073.1 1173.1 1273.1 1273.1 1333.1 density (kg/m3) 0.1787 specific he (J/kg-K) 5193 Water Tem (°F) 300 315 325 335 345 355 365 375 385	100.1 200.1 300.1 300.1 400.1 500.1 600.1 700.1 800.1 1000.1 1060.1 1060.1 (lbm/in3) 6.46E-06 eat (@tu/lbm-°F) 3 1.24	212.18 392.18 572.18 932.18 1112.18 1122.18 1472.18 1652.18 1832.18 1940.18	k (Btu/s-in-°F) 8.20E-06 8.48E-06 8.97E-06 9.06E-06 9.18E-06	2.345E-06 2.798E-06 3.078E-06 3.437E-06 4.242E-06 4.578E-06 5.356E-06 5.653E-06 5.804E-06 Cp (J/g-°C) 4.179 4.182 4.186 4.191 4.199 4.209 4.232	Cp (Btu/lbm-°F) 0.998 0.998 0.999 1.000 1.001 1.003 1.005 1.008 1.011	h (Btu/s-in ² -°F) 5.863E-05 6.996E-05 7.695E-05 8.591E-05 9.682E-05 1.060E-04 1.144E-04 1.339E-04 1.413E-04 1.451E-04 Density (g/cm3) 0.997 0.991 0.982 0.977 0.971 0.963 0.957 0.950	Density (lbm/in3) 0.036 0.036 0.035 0.035 0.035 0.035 0.035
T(K) 373.1 473.1 573.1 673.1 673.1 773.1 1073.1 1173.1 1273.1 1273.1 1333.1 density (kg/m3) 0.1787 specific he (J/kg-K) 5193 Water Tem (°F) 300 315 325 335 345 355 365 375 385 390	100.1 200.1 300.1 300.1 400.1 500.1 600.1 700.1 800.1 1000.1 1060.1 1060.1 (lbm/in3) 6.46E-06 eat (Btu/lbm-°F) 1.24 52 62 72 82 92 102 112 117	212.18 392.18 572.18 932.18 1112.18 112.18 1292.18 1652.18 1652.18 1832.18 1940.18	k (Btu/s-in-°F) (Btu/s-in-°F) (Btu/s-in-°F) (Btu/s-in-°F) (8.63E-06 8.63E-06 9.06E-06 9.18E-06 9.19E-06 9.19E-06	2.345E-06 2.798E-06 3.078E-06 3.437E-06 4.242E-06 4.578E-06 5.356E-06 5.653E-06 5.804E-06 5.804E-06 4.179 4.179 4.182 4.186 4.191 4.199 4.209 4.220 4.232 4.232	Cp (Btu/lbm-°F) 0.998 0.998 0.998 0.998 0.998 0.998 0.998 0.998 0.998 0.1001 1.003 1.005 1.008 1.011 1.012	Density (g/cm3) 0.997 0.991 0.982 0.997 0.991 0.963 0.995	Density (lbm/in3) 0.036 0.036 0.035 0.035 0.035 0.035 0.035
T(K) 373.1 473.1 573.1 673.1 673.1 1073.1 1173.1 1173.1 1273.1 1333.1 density (kg/m3) 0.1787 specific he (J/kg-K) 5193 Water Tem (°F) 300 315 325 335 345 365 375 385 365 375 3890 400	100.1 200.1 300.1 400.1 500.1 600.1 700.1 1000.1 1000.1 1000.1 1060.1 10	212.18 392.18 572.18 932.18 1112.18 1292.18 14772.18 1652.18 1832.18 1940.18	0.1753 0.2092 0.2301 0.2569 0.2895 0.3171 0.3422 0.3661 0.4004 0.4226 0.4339 k (Btu/s-in-°F) (Btu/s-in-°F) 8.20E-06 8.48E-06 8.63E-06 8.77E-06 9.9E-06 9.11E-06 9.19E-06 9.22E-06	2.345E-06 2.798E-06 3.078E-06 3.437E-06 4.242E-06 4.578E-06 5.356E-06 5.653E-06 5.804E-06 5.804E-06 4.179 4.179 4.182 4.186 4.191 4.199 4.209 4.220 4.232 4.232 4.232 4.232	Cp (Btu/lbm-°F) 0.998 0.998 0.998 0.998 0.998 0.998 0.998 0.999 1.000 1.001 1.003 1.005 1.008 1.011 1.012 1.016	Density (g/cm3) 0.997 0.991 0.982 0.977 0.950 0.945 0.937	Density (lbm/in3) 0.036 0.035 0.035 0.035 0.035 0.035 0.034
373.1 473.1 473.1 573.1 673.1 773.1 873.1 1073.1 1173.1 1273.1 1273.1 1273.1 1273.1 1273.1 Water Tem (°F) 300 315 325 345 355 365 375 385 390 400 410	100.1 200.1 300.1 300.1 400.1 500.1 600.1 700.1 800.1 900.1 1000.1 1060.	k (W/cm-°C) 6.13E-03 6.86E-03 6.86E-03 6.88E-03 6.88E-03 6.88E-03 6.88E-03 6.88E-03 6.88E-03 6.88E-03	k (Btu/s-in-°F) (Btu/s-in-°F) 8.20E-06 8.48E-06 8.77E-06 8.93E-06 9.06E-06 9.11E-06 9.18E-06 9.22E-06	2.345E-06 2.798E-06 3.078E-06 3.437E-06 4.242E-06 4.578E-06 5.356E-06 5.653E-06 5.804E-06 5.804E-06 4.179 4.186 4.191 4.199 4.209 4.232 4.232 4.232 4.239 4.256 4.278	Cp (Btu/lbm-°F) 0.998 0.999 1.000 1.001 1.003 1.005 1.005 1.005 1.005 1.005 1.005 1.005 1.005 1.005 1.006 1.001 1.002	Density (g/cm3) 0.997 0.991 0.982 0.997 0.950 0.945 0.995 0.	Density (lbm/in3) 0.036 0.035 0.035 0.035 0.035 0.035 0.034 0.034
T(K) 373.1 473.1 573.1 673.1 673.1 773.1 1073.1 1173.1 1273.1 1273.1 1333.1 density (kg/m3) 0.1787 Specific he (J/kg-K) 5193 Water Tem (°F) 300 315 325 335 345 355 365 375 385 390 400 410 420	100.1 200.1 300.1 300.1 400.1 500.1 600.1 700.1 800.1 1000.1 1060.1 1060.1 (lbm/in3) 6.46E-06 eat (Btu/lbm-°F) 3 1.24 52 62 72 82 92 102 112 117 127 137 147	212.18 392.18 572.18 932.18 1112.18 1122.18 1472.18 1652.18 1832.18 1940.18 (W/cm-°C) 6.13E-03 6.34E-03 6.45E-03 6.68E-03 6.71E-03 6.81E-03 6.86E-03 6.88E-03 6.88E-03 6.88E-03 6.88E-03	k (Btu/s-in-°F) 8.20E-06 8.48E-06 8.77E-06 8.97E-06 9.18E-06 9.19E-06 9.22E-06 9.22E-06	2.345E-06 2.798E-06 3.078E-06 3.437E-06 4.242E-06 4.578E-06 5.356E-06 5.653E-06 5.804E-06 5.804E-06 4.179 4.179 4.182 4.186 4.191 4.199 4.209 4.232 4.232 4.233 4.256 4.278 4.302	Cp (Btu/lbm-°F) 0.998 0.998 0.998 0.998 0.998 0.999 1.000 1.001 1.003 1.005 1.008 1.012 1.016 1.022 1.027	Density (g/cm3) 0.997 0.991 0.982 0.977 0.950 0.945 0.997 0.999 0.919	Density (lbm/in3) 0.036 0.036 0.035 0.035 0.035 0.035 0.034 0.034 0.034 0.034

Axial heat load distribution in annulus:

.

$$q_{total} := 6135 \,\mathrm{W}$$

Total heating rate in tube

$$D_0 := 3.446 \text{ in}$$

Outside diameter of tube

$$D_i := D_0 - 0.06 in$$

Inside diameter of tube

$$D_i = 3.386in$$

$$A_W := \frac{\pi}{4} \cdot \left(D_o^2 - D_i^2 \right)$$

Cross-sectional area of tube

$$\textbf{q}_{w} \coloneqq \frac{0.5 \cdot \textbf{q}_{total}}{\textbf{A}_{w} \cdot \Delta \textbf{x}} \cdot \frac{\textbf{P}_{norm}}{\sum \textbf{P}_{norm}}$$

$$q_{w} = \begin{pmatrix} 0.528 \\ 0.499 \\ 0.444 \\ 0.365 \\ 0.267 \\ 0.154 \end{pmatrix} \frac{1}{s} \frac{BTU}{in^{3}}$$

$$q_{avg} := \frac{q_{total}}{A_w \cdot 48 \cdot in}$$

$$q_{avg} = 0.376 \frac{1}{s} \frac{BTU}{in^3}$$

$$\mathbf{q}_{\mathbf{w}} := \mathbf{q}_{\mathbf{avg}} \!\cdot\! \mathbf{P}_{\mathbf{norm}}$$

$$q_{W} = \begin{pmatrix} 0.527 \\ 0.499 \\ 0.444 \\ 0.365 \\ 0.267 \\ 0.154 \end{pmatrix} \frac{1}{s} \frac{BTU}{in}$$

Axial heat load distribution in Water Channels.

 $q_{\text{total}} := 3860\,\text{W}$

Total heating rate

 $D_{\text{water}} := .25 \cdot \text{in}$

Outside diameter of tube

 $A_w := \frac{\pi}{4} \cdot D_{water}^2$

Cross-sectional area of tube

$$A_{W} = 0.049in^{2}$$

 $q_{w} \coloneqq \frac{0.5 \cdot q_{total}}{A_{w} \cdot \Delta x} \cdot \frac{P_{norm}}{\sum P_{norm}}$

$$q_{W} = \begin{pmatrix} 2.2 \\ 2.1 \\ 1.8 \\ 1.5 \\ 1.1 \\ 0.6 \end{pmatrix} \frac{1}{s} \frac{BTU}{in^{3}}$$

$$q_{avg} := \frac{q_{total}}{A_w \cdot 48 \cdot in}$$

$$q_{avg} = 1.553 \frac{1}{s} \frac{BTU}{in^3}$$

$$\mathbf{q}_{\mathbf{W}} := \mathbf{q}_{\mathbf{avg}} \!\cdot\! \mathbf{P}_{\mathbf{norm}}$$

$$q_{W} = \begin{pmatrix} 2.175 \\ 2.058 \\ 1.831 \\ 1.506 \\ 1.101 \\ 0.636 \end{pmatrix} \frac{1}{s} \frac{BTU}{in^{3}}$$

Axial heat load distribution in envelope tube.

 $q_{\text{total}} := 70500\,\text{W}$

Total heating rate in tube

 $D_i := 3.776 in$

Inside diameter of tube

 $D_0 := 4.026 \text{ in}$

Outside diameter of tube

 $A_W := \frac{\pi}{4} \cdot \left(D_o^2 - D_i^2 \right)$

Cross-sectional area of tube

$$q_{w} \coloneqq \frac{0.5 \cdot q_{total}}{A_{w} \cdot \Delta x} \cdot \frac{P_{norm}}{\sum P_{norm}}$$

$$q_{W} = \begin{pmatrix} 1.3 \\ 1.2 \\ 1.1 \\ 0.9 \\ 0.6 \\ 0.4 \end{pmatrix} \frac{1}{s} \frac{BTU}{in^{3}}$$

$$q_{avg} := \frac{q_{total}}{A_w \cdot 48 \cdot in}$$

$$q_{avg} = 0.909 \frac{1}{s} \frac{BTU}{in^3}$$

$$q_{w} := q_{avg} \cdot P_{norm}$$

$$q_{W} = \begin{pmatrix} 1.273 \\ 1.205 \\ 1.072 \\ 0.882 \\ 0.644 \\ 0.372 \end{pmatrix} \frac{1}{s} \frac{BTU}{in}$$

Axial heat load distribution in pressure tube.

 $q_{total} := 58320 \,\mathrm{W}$

Total heating rate in tube

 $D_i := 3.446 in$

Inside diameter of tube

 $D_0 := 3.696 \text{ in}$

Outside diameter of tube

 $A_{w} := \frac{\pi}{4} \cdot \left(D_{o}^{2} - D_{i}^{2} \right)$

Cross-sectional area of tube

 $q_{w} \coloneqq \frac{0.5 \cdot q_{total}}{A_{w} \cdot \Delta x} \cdot \frac{P_{norm}}{\sum P_{norm}}$

Heating rate in tube axial segments

 $q_{W} = \begin{pmatrix} 1.2 \\ 1.1 \\ 1 \\ 0.8 \\ 0.6 \\ 0.3 \end{pmatrix} \frac{1}{s} \frac{BTU}{in^{3}}$

$$q_{avg} := \frac{q_{total}}{A_w \cdot 48 \cdot in}$$

$$q_{avg} = 0.821 \frac{1}{s} \frac{BTU}{in^3}$$

$$q_w := q_{avg} \cdot P_{norm}$$

$$q_{W} = \begin{pmatrix} 1.15\\ 1.088\\ 0.969\\ 0.797\\ 0.582\\ 0.336 \end{pmatrix} \frac{1}{s} \frac{BTU}{in}$$

Axial heat load distribution in Al-Hf alloy.

 $q_{total} := 40300 \,\mathrm{W}$

Total heating rate in tube

 $D_{pt} := 3.446 in$

Inside diameter of tube

 $D_{expt} := 1.25 in$

Outside diameter of tube

 $D_{\text{water}} := 0.25 \text{ in}$

 $A_{w} := \frac{\pi}{4} \cdot \left(D_{pt}^{2} - 3.D_{expt}^{2} - 4 \cdot D_{water}^{2} \right)$

Cross-sectional area of heat sink

 $A_{W} = 5.449in^{2}$

 $q_{w} \coloneqq \frac{0.5 \cdot q_{total}}{A_{w} \cdot \Delta x} \cdot \frac{P_{norm}}{\sum P_{norm}}$

$$q_{w} = \begin{pmatrix} 0.205 \\ 0.194 \\ 0.172 \\ 0.142 \\ 0.104 \\ 0.06 \end{pmatrix} \frac{1}{s} \frac{BTU}{in^{3}}$$

$$q_{avg} := \frac{q_{total}}{A_w \cdot 48 \cdot in}$$

$$q_{avg} = 0.146 \frac{1}{s} \frac{BTU}{in^3}$$

$$q_{w} := q_{avg} \cdot P_{norm}$$

$$\mathbf{q_W} = \begin{pmatrix} 0.205 \\ 0.194 \\ 0.172 \\ 0.142 \\ 0.104 \\ 0.06 \end{pmatrix} \frac{1}{s} \frac{\mathbf{BTU}}{\mathbf{in}^3}$$

Axial heat load distribution from fuel - surface heat flux.

 $\mathsf{q}_{\text{total}} := 70000\,\mathrm{W}$

Total heating rate in each fuel tube

length := $4 \cdot in$

 $D_0 := 1.25 \text{ in}$

Outside diameter of tube

 $A_{\mathbf{W}} := \pi \cdot D_{\mathbf{O}} \cdot \text{length}$

Cross-sectional area of tube

 $q_{w} \coloneqq \frac{0.5 \cdot q_{total}}{A_{w}} \cdot \frac{P_{norm}}{\sum P_{norm}}$

Heating rate in tube axial segments

 $q_{W} = \begin{pmatrix} 0.493 \\ 0.467 \\ 0.416 \\ 0.342 \\ 0.25 \\ 0.144 \end{pmatrix} \frac{1}{s} \frac{BTU}{in^{2}}$

$$q_{avg} := \frac{q_{total}}{12A_W}$$

$$q_{avg} = 0.4 \frac{1}{s} \frac{BTU}{in^2}$$

$$\mathbf{q}_{\mathbf{w}} \coloneqq \mathbf{q}_{\mathbf{avg}} {\cdot} \mathbf{P}_{\mathbf{norm}}$$

$$q_{W} = \begin{pmatrix} 0.493 \\ 0.467 \\ 0.415 \\ 0.341 \\ 0.25 \\ 0.144 \end{pmatrix} \frac{1}{s} \frac{BTU}{in^{2}}$$

Hydraulic Analysis - 1/4 inch coolant channels

$$D_h := 0.25 in$$

$$g = 9.807 \frac{m}{s^2}$$

Length := 48·in

$$P := 4.964210^5 \cdot Pa$$

Area :=
$$\frac{\pi}{4} \cdot D_h^2$$

$$\epsilon := 1.31 \times \ 10^{-6} m$$

$$\varepsilon = 5.157 \times 10^{-5}$$
 in

$$p := \frac{\epsilon}{D_L}$$

$$p = 2.063 \times 10^{-4}$$

Guess velocity:

$$vel := 15.4 \frac{m}{s}$$

$$v:=2.48\times\ 10^{-3}\cdot\frac{cm^2}{s} \qquad \qquad \rho:=950\frac{kg}{m}$$

$$\rho := 950 \frac{\text{kg}}{3}$$

Compute Reynolds number:

$$\text{Re}_d := \frac{\text{vel} \cdot \text{D}_h}{\nu}$$

Compute friction factor:

$$fx := -1.8 \log \left[\left(\frac{p}{3.7} \right)^{1.11} + \frac{6.9}{Re_d} \right]$$

$$ff := \frac{1}{fx^2}$$

Calculate loss coefficient:

$$K_{maj} \! \coloneqq \! ff \! \cdot \! \frac{Length}{D_h}$$

$$K_{ent} := 0.5$$

$$K_{exit} = 1.0$$

$$K_{tot} := K_{maj} + K_{ent} + K_{exit}$$
 $K_{tot} = 4.509$

$$K_{tot} = 4.509$$

Calculate flow rate:

$$Q := Area \cdot \sqrt{\frac{2}{K_{tot}} \cdot \left(g \cdot Length + \frac{P}{\rho}\right)} \qquad \qquad Q = 4.876 \times \ 10^{-4} \ \frac{m^3}{s} \qquad \qquad Q = 7.729 gpm$$

$$Q = 4.876 \times 10^{-4} \frac{m^3}{s}$$

$$vel2 := \frac{Q}{Area}$$

$$vel2 = 15.398 \frac{m}{s}$$

$$Vol = 3.861 \times 10^{-5} \text{ m}^3$$

$$Vol_{tot} := 4 \cdot Vol$$

$$Vol_{tot} = 1.544 \times 10^{-4} \text{ m}^3$$

Gamma heating:

$$q_{gamma} := 3 \cdot \left(8.5 \cdot \frac{W}{gm}\right) \cdot \rho \cdot Vol_{tot}$$

$$q_{\text{gamma}} = 3.741 \times 10^3 \,\text{W}$$

APPENDIX B ALTERNATE THERMAL CALCULATIONS

Presented here are temperature distributions calculated for the alternate thermal configuration analyzed, having additional heat load from the experiment chambers. Thermal analysis was performed considering a total heat load of 384 kW from the three experiment chambers. Similar temperature distributions with elevated magnitudes are seen in the system components. The maximum temperature (306.4 °C, 583.5 °F) occurs in the hafnium aluminum absorber. Under nominal operating conditions, the calculated FIR and DNBR under nominal operating conditions are 4.4 and 4.6, respectively, which exceed the minimum value of 2.

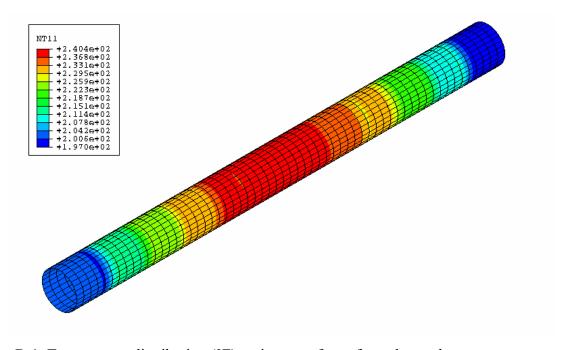


Figure B-1. Temperature distribution (°F) on inner surface of envelope tube.

APPENDIX B

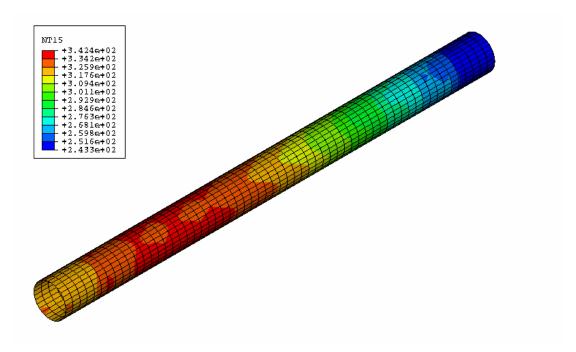


Figure B-2. Temperature distribution (°F) on outer surface of pressure tube.

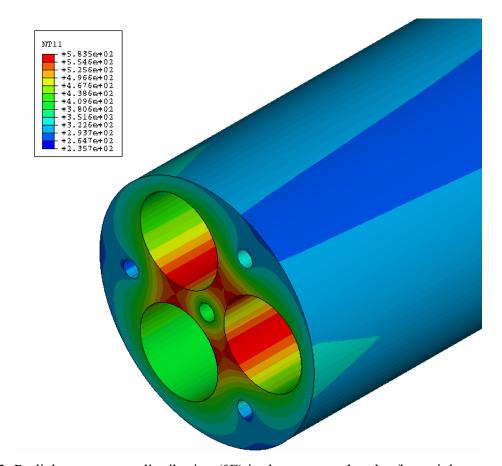


Figure B-3. Radial temperature distribution (°F) in the neutron absorber/heat sink.

APPENDIX B

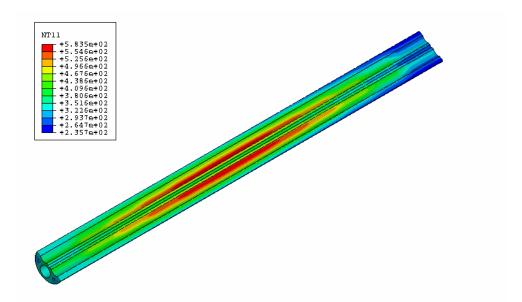


Figure B-4. Axial temperature distribution (°F) in the hafnium aluminum absorber.

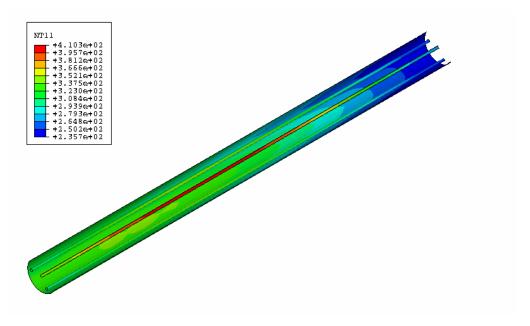


Figure B-5. Temperature distribution (°F) in the oxide layers.

APPENDIX B

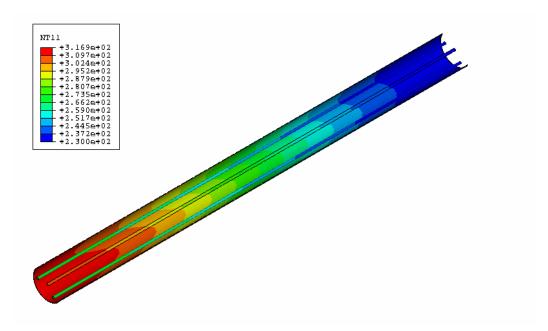


Figure B-6. Temperature distribution (°F) in the water coolant.

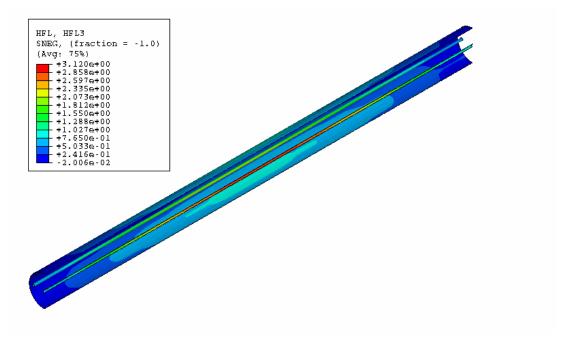


Figure B-7. Distribution of surface heat flux (BTU/s-in²) at the oxide surfaces.

APPENDIX C TOTAL PROJECT COST SUMMARY

Presented here is the Total Project Cost Summary Report for the BFFL alternate cooling concept for the fast flux test capability in the ATR.

TPC Summary Report

Project Name: Boosted Fast Flux Loop

Rounded TPC (Rounded to the nearest \$ 100000)

Project Location: INL - RTC Advanced Test Reactor Project Number: 7A48

TOTAL ESTIMATE ELEMENT Estimate Subtotal Escalation Contingency 12.59% \$2,265,066 25.00% \$5,064,015 Total Estimated Cost (TEC) \$17,990,993 \$25,320,074 25.00% \$7,617,443 12.59% \$3,407,180 Other Project Cost (OPC) \$27,062,592 \$38,087,215 12.59% \$5,672,246 25.00% \$12,681,458 Total Project Cost (TPC) \$45,053,585 \$63,407,289

	Remarks
Type of Estimate: Class 4	
Estimator: B. W. Wallack MS 3204, 526-5896	
Checked By:	_
Approved By: Will EWOYND 8/20/07-	

BEA

08/13/2007 16:04:54 Jaho National Laboratory

Cost Estimating

Page No.

\$63,400,000

Battelle Energy Alliance (BEA)

COST ESTIMATE SUPPORT DATA RECAPITULATION

Project Title:

Boosted Fast Flux Loop

Estimator:

B. W. Wallace

Date:

August 13, 2007

Estimate Type: Class 4

File:

7A48

Approved By:

Page 1 of 5

I. PURPOSE: Brief description of the intent of how the estimate is to be used, i.e., for engineering study, comparative analysis, DWP, LCB out-year planning, BCP, etc.

The purpose of this cost estimate is to establish a rough order of magnitude (ROM) planning value of the Boosted Fast Flux Loop project for use by the Department of Energy in decision making of path forward for this and similar projects.

II. SCOPE OF WORK: Brief statement of the project's objective. Thorough overview and description of the proposed project. Identify work to be accomplished, as well as any specific work to be excluded.

The objective of this project is to design and install a capability in the existing Advanced Test Reactor Facility (ATR) that will provide the test environment necessary for the irradiation testing of advanced reactor fuels and materials requiring an intense fast neutron flux.

The scope of work to achieve the objectives for this project includes research and development, engineering, modifications to certain safety basis and procedures, design, installation, testing, and qualification of the booster fuel.

This estimate specifically excludes:

- Any life cycle costs after the loop has been accepted for operations.
- В. Shipment of the irradiated booster fuel elements from the ATR to INTEC.
- Any necessary changes to equipment, procedures, safety basis, etc., supporting the C. shipment of irradiated booster fuel elements from the ATR to INTEC.
- Costs for the customer to prepare, install and handle test trains. D.
- E. Additional ATR fuel purchase and handling in support of the boosted fast flux loop.
- Any costs or expenditures prior to the beginning of FY 2008. F.
- G. Management administration and analysis required to move the project to CD1.
- III. BASIS OF THE ESTIMATE: Overall methodology and rationale of how the estimate was developed. Source documents to include drawings, design reports, engineers' notes and/or other documentation upon which the estimate is originated. Overall explanation of sources for resource pricing.

COST ESTIMATE SUPPORT DATA RECAPITULATION

Continued –

Project Title: Boosted Fast Flux Loop

File: 7A48 Page 2 of 5

This cost estimate is based on Cost Estimating file #7367-B performed on September 8, 2005. The revisions reflected in this estimate are based on input from the project team in a meeting held on July 24, 2007. Cost Estimating file #7367-B was based upon numerous meetings with the project team, input from the project, and the "Gas Test Loop Conceptual Design: 70% Progress Report" dated March 2005.

- IV. <u>ASSUMPTIONS</u>: Condition statements accepted or supposed true without proof of demonstration; statements adding clarification to scope. An assumption has a direct impact on total estimated cost.
 - A. A performance period addressing CD1 approval through project turnover, beginning in fiscal year 2009 and extending through fiscal year 2012 has been identified for the project.
 - B. There will be no changes to the attractiveness levels of the special nuclear facilities.
 - C. Customers will provide all transportation of experimental material to the INL. Onsite transportation of experiments, before and after irradiation, will be included in each experiment's operational cost.
 - D. The booster fuel will perform as designed in one run and will not require any re-engineering or additional runs.
 - E. The NMIS storage racks will be constructed of non-combustible materials.
 - F. The irradiated single plate specimens will be transported from the ATR to the MFC for the post irradiation examination (PIE) in an appropriate cask under a transport plan authorization.
 - G. The single plate specimens will remain at the MFC for disposal once the PIE has been completed. The cost for this disposal at the MFC has been included in the PIE costs.
 - H. There will be no significant equipment changes or modifications to the ATR unless otherwise stated within the body of this estimate.
 - I. System will be designed to support three individual test trains. Each test train space will be designed for five capsules each with supporting control gas and instrumentation to support these 15 individual specimen environments.
 - J. Three dummy test trains with minimal instrumentation to support system operational testing will be developed and installed.
 - K. One third of the spare mechanical components are covered by this estimate, the remaining two thirds are considered life cycle costs.
 - L. BWXT can successfully fabricate the single plate specimens.
 - M. The booster fuel can be qualified.
 - N. The Boosted Fast Flux Loop System will consist of a single gas system; the "Specimen Environment Control and Sample Carrier System" primarily used as temperature and environmental control of the experiment.

COST ESTIMATE SUPPORT DATA RECAPITULATION

Continued –

Project Title: Boosted Fast Flux Loop

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O. Primary heat removal will be performed using the existing pressurized water system at ATR. It is assumed and reflected in the estimate that this system will be available for use by this project.

- P. The sample system associated with the "Specimen Environment Control and Sample Carrier System" will be specific to the test sponsor needs and will not be part of this design. Concepts for the sample system will be considered and adequate space and adaptability will be provided in the design to allow for future additions. The distribution system will be designed such that the sample system can easily be integrated into the system in the future.
- Q. The majority of the gas system mechanical equipment will be located in shielded Cubicle 2E and in the surrounding area of this cubicle within the ATR second basement. It is assumed adequate space is available in the shielded cubicle for equipment that has the potential of being a radiation source.
- R. The flow rates, pressure requirements, and gas media for the "Specimen Environment Control and Sample Carrier System" will be comparable to other "Instrumented Lead" type experiments that have previously been conducted at ATR. The gas blend will be made up of helium and neon.
- S. From previous test experience it is estimated that the flow rate for the "Specimen Environment Control and Sample Carrier System" will be around 60 sccm at system inlet pressure of less than 50 psi. The system will be designed as a single pass system; the gas blend exiting the experiment capsule will be delayed, as appropriate for fission product decay, and then will be released to the ATR stack.
- T. It is estimated that the "Boosted Fast Flux Loop" will be required to remove approximately 200 kW from the experiment area.
- U. Further analysis associated with specific experiment design, allowable capsule temperatures, and actual heat loads, will need to be performed to determine the actual gas flow parameters. Also, methods will be used to optimize the experiment capsule design for heat transfer and to minimize the required gas flow rate.
- V. Adequate high and low pressure demineralized water will be provided from existing ATR systems.
- W. Gas Purification/Filtration will be provided for clean up of the "Boosted Fast Flux Loop" gas if it becomes contaminated.
- X. The gas supply, gas quality, mass flow indication/control and mixing, and gas purification sub-systems of the "Specimen Environment Control and Sample Carrier System" will not require shielding and will be located in available space surrounding the shielded cubicle.
- Y. The control system will be similar to that in use for other testing programs. It will be independent from existing ATR communications systems and control system networks. The control system consists of vendor-supplied distributed control system (DCS) components, hardware and software, uninterruptible power supply and system power, thermocouple readouts and associated cabling, and process input and output cabling.

COST ESTIMATE SUPPORT DATA RECAPITULATION

Continued –

Project Title: Boosted Fast Flux Loop

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- Z. The temperature control system will be capable of displaying the temperature within each capsule. The control system and associated work station will be located in the corridor near the shielded cubicle.
- AA. There will be methods available for experiment handling capability, before and after irradiation, as part of transportation interfaces at the ATR.
- BB. An acceptable technique, such as leak-before-break technology, can be readily (without significant R&D) developed and incorporated into the Advanced Test Reactor safety basis to justify sustained long-term reactor operation at the increased lobe power necessary to support the boosted fast flux loop fast neutron flux objective.
- CC. The Boosted Fast Flux Loop can be operated with dummy booster fuel elements instead of actual booster fuel elements in situations not requiring the irradiation benefits of actual booster fuel.
- V. <u>CONTINGENCY GUIDELINE IMPLEMENTATION</u>: Explanation of methodology used in determining overall contingency. Identify any specific drivers or items of concern.

At this time this project contains 25% contingency as determined by the requester and the project team. Some areas of concern for this project include:

- A. This never performed work represents research and development activities. The ability for success of this project is contingent on the theories as laid out in the conceptual design at this time.
- B. Single plate specimens will be irradiated in one of the ATR Flux Traps, visually inspected, and, after cooling, sent to HFEF for PIE. The possibility of needed design modifications may require a second round of single plate specimen irradiation testing, but costs for that are not in the estimate.
- C. Success, as gauged by the visual evaluation of the mini plate test, would support CD-1, allowing design to start. Final verification of performance of the loop will not be obtained until after the testing of the loop in the ATR.
- D. Main booster fuel assembly development would start with success in single plate testing. Parts of that development would be delayed if failure was evident in the first single-plate specimen test.
- E. Results from the single plate test can impact the schedule.
- F. The project would be accepted with completion of visual examination of complete booster fuel elements after testing in ATR. The need to perform PIE on those elements is not foreseen or budgeted.
- G. Limited resources could delay or increase the cost of the project.
- H. ATR operational issues can directly impact the project.
- The operation of the Boosted Fast Flux Loop changes the operation of the ATR.
 Higher power and shorter run times may impact the safety analysis.

COST ESTIMATE SUPPORT DATA RECAPITULATION

Continued –

Project Title: Boosted Fast Flux Loop

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J. Should there be no methods for the experiment handling capability, before and after irradiation, as part of transportation interfaces at the ATR, costs could increase.

VI. <u>ESTIMATE SUMMARY</u>: Total dollars/hours and Rough Order Magnitude (ROM) allocations of the methodologies used to develop the cost estimate.

Estimate Methodology	ROM Percentage %
Project Team	100
Recorded Actuals	0
Parametric	0
Vendor Quotes	0
Other	0
TOTAL	100

VII. OTHER COMMENTS/CONCERNS SPECIFIC TO THE ESTIMATE:

- A. All labor resources reflect current burdened BEA labor rates.
- B. Escalation for the project reflects a March midpoint of 2011.

Project Summary Report

Client: W. D. Ridgway, MS 3750, 526-4790
Prepared By: B. W. Wallace, MS 3204, 526-5896
Estimate Type: Class 4

Project Name: Boosted Fast Flux Loop

Project Location: INL - RTC Advanced Test Reactor Estimate Number: 7A48

Level	Description	Estimate Subtotal	Escalation	Contingency	Contingency	TOTAL	
OPC1000	Project Management and Support During Operational Activities	\$4,221,770	\$531,521	\$1,188,323	25.00%	\$5,941,614	
OPC1000.10	Project Management, Administration , and Analysis Prior to CD1	\$1,022,600	\$128,745	\$287,836	25.00%	\$1,439,182	
OPC1000.20	Project Management and Support During Operational Activities	\$3,199,170	\$402,776	\$900,486	25.00%	\$4,502,432	
OPC2000	Develop RTC Facilities Safety Analysis for the GTL	\$4,003,816	\$504,080	\$1,126,974	25.00%	\$5,634,870	
OPC3000	Operating Procedures	\$4,811,821	\$605,808	\$1,354,407	25.00%	\$6,772,037	
OPC3000.10	Management Self Assessment (MSA)	\$648,655	\$81,666	\$182,580	25.00%	\$912,901	
OPC3000.20	Documentation for the GTL System and Misc. Expenses	\$2,637,067	\$332,007	\$742,269	25.00%	\$3,711,343	
OPC3000.30	Operating Procedures for the GTL System	\$1,526,099	\$192,136	\$429,559	25.00%	\$2,147,793	
CAP1000	Project Management and Support During Capital Activities	\$3,649,097	\$459,421	\$1,027,130	25.00%	\$5,135,648	
OPC4000	Booster Fuel	\$8,360,226	\$1,052,552	\$2,353,195	25.00%	\$11,765,973	
OPC4000.10	Technical Committee Review	\$131,262	\$16,526	\$36,947	25.00%	\$1 84,735	
OPC4000.30	Plate Specimen Fabrication @ BWXT	\$340,668	\$42,890	\$95,890	25.00%	\$479,448	
OPC4000.40	Booster Fuel Fabrication	\$478,462	\$60,238	\$ 134,675	25.00%	\$673,376	
OPC4000.40.10	Fabricate the Booster Fuel Elements & Dummies	\$385,074	\$48,481	\$108,389	25.00%	\$541,943	
OPC4000.40.20	Oversight of the Booster Fuel Fabrication	\$93,388	\$11,758	\$26,286	25.00%	\$131,432	
OPC4000.50	Shipment of the Plate Specimens	\$409,833	\$51,598	\$115,358	25.00%	\$576,789	
OPC4000.50.10	Ship Fresh Fuel Plate Specimens from BWXT to ATR	\$108,612	\$13,674	\$30,572	25.00%	\$152,858	
OPC4000.50.20	Ship Irradiated Fuel Plate Specimens from ATR to MFC for PIE	\$301,221	\$37,924	\$84,786	25.00%	\$423,931	
OPC4000.50.20.10	(A) Standard Hazardous Category 2 Transport Plan	\$214,784	\$27,041	\$60,456	25.00%	\$302,282	
OPC4000.50.20.20	(E) Loading Operations at ATR	\$51,074	\$6,430	\$14,376	25.00%	\$71,881	
OPC4000.50.20.30	(B) Standard Transport Operating Cost for Transporting Under A Transport Plan	\$7,801	\$982	\$2,196	25.00%	\$10,979	
OPC4000.50.20.40	(F) Unloading Operations at MFC/HFEF	\$27,561	\$3,470	\$7,758	25.00%	\$38,789	
OPC4000.80	Booster Fuel Element Irradiation Unit (IU) Charges @ RTC	\$7,000,000	\$881,300	\$1 ,970,3 2 5	25.00%	\$9,851,625	
OPC4100	Nuclear Testing	\$2,861,199	\$360,225	\$805,356	25.00%	\$4,026,780	
OPC4100.20	ATRC Testing for BFFL System	\$453,099	\$57,045	\$127 ,536	25.00%	\$637,680	

BEA

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Project Summary Report

Project Name: Boosted Fast Flux Loop

Client: W. D. Ridgway, MS 3750, 526-4790
Prepared By: B. W. Wallace, MS 3204, 526-5896
Estimate Type: Class 4 Project Location: INL - RTC Advanced Test Reactor Estimate Number: 7A48 Contingency

					Contingency		
Level OPC4100.30	Description EATRC Testing for the Plate Specimens	stimate Subtotal \$306,924	Escalation \$38,642	Contingency \$86,391	<u>%</u> 25.00%	TOTAL \$431,957	
OPC4100.40	Plate Specimens Section Testing in ATR Flux Trap	\$1,101,177	\$138,638	\$309,954	25.00%	\$1,549,768	
OPC4100.50	Plate Specimen Irradiation Unit (IU) Charges @ RTC	\$1,000,000	\$12 5,900	\$281,475	25.00%	\$1,407,375	
OPC5000	Hafnium-Aluminum Block Development/Production	\$1,257,842	\$158,362	\$354,051	25.00%	\$1,770,255	
OPC5000.10	Hafnium-Aluminum Block Development/Production	\$1,257,842	\$158,362	\$354,051	25.00%	\$1,770,255	
CAP4000	ATR Gas System and Hardware	\$12,777,509	\$1,608,688	\$3,596,549	25.00%	\$17,982,747	
CAP4000.05	Captial Design	\$4,481,963	\$564,279	\$1,261,561	25.00%	\$6,307,803	
CAP4000.10	Project Analyses	\$2,189,723	\$275,686	\$616,352	25.00%	\$3,081,762	
CAP4000.20	System Testing	\$477,876	\$60,165	\$134,510	25.00%	\$672,551	
CAP4000.40	$\dots. {\sf Temperature\ Control}, \textbf{S} \textbf{ampling\ System, and\ He\ Monitoring\ and\ Insulation\ G}$	Sap \$1,796,371	\$226,163	\$505,633	25.00%	\$2,528,167	
CAP4000.50	Electrical, Instrumentation and Control Systems	\$2,711,697	\$341,403	\$763,275	25.00%	\$3,816,375	
CAP4000.60	Tank Hardware	\$718,187	\$90,420	\$202,152	25.00%	\$1,010,758	
CAP4000.70	\ldots . Modifications for Installation of the GTL in a Corner Lobe	\$401,692	\$50,573	\$113,066	25.00%	\$565,331	
CAP5000	Facility Modifications	\$967,933	\$121,863	\$272,449	25.00%	\$1,362,245	
CAP5000.10	Racks @ NMIS	\$143,239	\$18,034	\$40,318	25.00%	\$201,591	
CAP5000.30	Canal Fuel Storage	\$824,694	\$103,829	\$232,131	25.00%	\$1,160,654	
OPC6000	<u>Operations</u>	\$477,906	\$60,168	\$134,519	25.00%	\$672,593	
OPC6000.10	Operations	\$477,906	\$60,168	\$134,519	25.00%	\$672,593	
OPC7000	Performance Testing	\$899,184	\$113,207	\$253,098	25.00%	\$1,265,490	
OPC7000.10	Execute the Performance Test	\$261,336	\$32,902	\$73,560	25.00%	\$367,798	
OPC7000.20	Plate Specimen Post Irradiation Examination (PIE) @ MFC	\$594,670	\$74,869	\$167,385	25.00%	\$836,924	
OPC7000.30	Canal Visual Examination (VE) of the Booster Fuel Elements	\$43,178	\$5,436	\$12,154	25.00%	\$60,768	
OPC8000	Other Operational Adders	\$168,828	\$21,255	\$47,521	25.00%	\$237,604	
OPC8000.10	BEA Material Handling and G&A Fees - Operational	\$64,536	\$8,125	\$18,165	25.00%	\$90,826	

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Project Summary Report

Project Name: Boosted Fast Flux Loop

Project Location: INL - RTC Advanced Test Reactor Estimate Number: 7A48

Total Boosted Fast Flux Loop

Client: W. D. Ridgway, MS 3750, 526-4790
Prepared By: B. W. Wallace, MS 3204, 526-5896
Estimate Type: Class 4

25.00%

\$63,407,289

\$5,672,246 \$12,681,458

					Contingency	
Level	Description	Estimate Subtotal	Escalation	Contingency	%	TOTAL
OPC8000.20	Project Acceptance and Closeout	\$104,292	\$13,130	\$29,356	25.00%	\$146,778
OPC8000.20.10	Records Disposition	\$27,549	\$3,468	\$7,754	25.00%	\$38,771
OPC8000.20.20	Material Disposition	\$6,513	\$820	\$1,833	25.00%	\$9,166
OPC8000.20.30	Complete Closeout PM Checklist	\$70,230	\$8,842	\$19,768	25.00%	\$98,840
CAP9000	Other Capital Adders	\$596,454	\$75,094	\$167,887	25.00%	\$839,435
CAP9000.10	BEA Material Handling and G&A Fees - Capital	\$596,454	\$75,094	\$167,887	25.00%	\$839,435

\$45,053,585

