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The goal of the EZturb mix model in KULL is to predict the turbulent mixing process as it evolves from Rayleigh-Taylor, Richtmyer-Meshkov, or Kelvin-Helmholtz instabilities. In this report we focus on a simple example of the Richtmyer-Meshkov instability (which occurs when a shock hits an interface between fluids of different densities) without the complication of reshock. The experiment by Benjamin et al. [1], involving a Mach 1.21 incident shock striking an air / $SF₆$ interface, is a good one to model and understand before moving onto shock tubes that follow the growth of the turbulent mixing zone from first shock through well after reshock [2-3].

In Kull, the EZturb k- ε model is tightly coupled to the Lagrange hydro, and so the actual mix model equations we solve when the model is active are:

$$
\frac{d\alpha_r}{dt} = \frac{\partial}{\partial x_j} \left(\frac{\mu_t}{\sigma_M} \frac{\partial}{\partial x_j} \left(\frac{\alpha_r}{\rho} \right) \right)
$$

$$
\frac{d\alpha_r \rho_r}{dt} = \frac{\partial}{\partial x_j} \left(\frac{\mu_t}{\sigma_M} \frac{\partial}{\partial x_j} \left(\frac{\alpha_r \rho_r}{\rho} \right) \right)
$$

$$
\frac{d\rho u_i}{dt} = -\frac{\partial \tau_{ij}}{\partial x_j}
$$

$$
\frac{d\alpha_r \rho_r I_r}{dt} = \frac{\partial}{\partial x_j} \left(\frac{\mu_t}{\sigma_U} \frac{\partial}{\partial x_j} \left(\frac{\alpha_r \rho_r I_r}{\rho} \right) \right) + P_r^I + \delta_{I, Diss} \alpha_r \rho_r \varepsilon
$$

$$
\frac{d\rho k}{dt} = \frac{\partial}{\partial x_j} \left(\frac{\mu_t}{\sigma_K} \frac{\partial k}{\partial x_j} \right) - \tau_{ij} S_{ij} - \rho \varepsilon + P
$$
\n
$$
\frac{d\rho \varepsilon}{dt} = \frac{\partial}{\partial x_j} \left(\frac{\mu_t}{\sigma_z} \frac{\partial \varepsilon}{\partial x_j} \right) - C_{1\varepsilon} \tau_{ij} S_{ij} \frac{\varepsilon}{k} - C_{2\varepsilon} \rho \frac{\varepsilon^2}{k} + C_{3\varepsilon} P \frac{\varepsilon}{k} .
$$

Here, α_r , ρ_r , and I_r are the volume fraction, thermodynamic density, and specific internal energy (by mass) for material r. S_{ij} is the strain rate tensor, and τ_{ij} is the turbulent shear stress tensor, for which we use the following Boussinesq approximation:

$$
\tau_{ij} = \delta_{lso} \frac{2}{3} \rho k \delta_{ij} - \delta_{Anso} 2\mu_t \left(S_{ij} - \frac{\delta_{ij}}{3} \frac{\partial u_k}{\partial x_k} \right) .
$$

The turbulent viscosity includes the effects of both shear and buoyancy and takes the form:

$$
\mu_t = C_\mu \rho \frac{k^2}{\varepsilon} + C_\omega \rho \frac{k^3}{\varepsilon^2} \sqrt{\omega^2 + \frac{\nabla p \cdot \nabla p}{p \rho} - \frac{\nabla p \cdot \nabla \rho}{\rho^2} \Big[1 - \Theta(\nabla p \cdot \nabla \rho) \Big]}.
$$

The unlimited form of the buoyant production term is given by:

$$
P = -\frac{\mu_t}{\sigma_{\rho} \rho^2} \nabla p \cdot \nabla \rho
$$

and the way this term manifests itself in the internal energy equation is:

$$
P_r^I = -h_r p_r \nabla \cdot \left(\frac{\mu_t}{\sigma_\rho \rho^2} \nabla \rho\right) .
$$

The model constants are $C_{1\varepsilon}$, $C_{2\varepsilon}$, $C_{3\varepsilon}$, σ_M , σ_U , σ_K , σ_Z , σ_ρ , C_μ , and C_ω . Also, δ_{Iso} , δ_{Aniso} , and $\delta_{\text{I,diss}}$ are on/off switches that can be set to 1 or 0. To simplify the form of the turbulent viscosity and the Reynolds stress, we will set $C_{\omega} = 0$ and $\delta_{\text{Aniso}} = 0$ for this problem.

We are given that the incident Mach number is 1.21 and that the ambient densities for the air and SF_6 are .9524e-3 g/cm³ and 4.8611e-3 g/cm³. The ambient pressure is also given as .8 bars. With these values and the standard 1D shock relations [4-5], we can compute shocked values for the air (we assume $\gamma_{\text{air}} = 1.4$). Thus the shocked air density, pressure, and velocity are found to be 1.294e-3 g/cm^3 , 1.233e6 dynes/cm², and 1.096e4 cm/sec. A spatial domain of 70 cm was selected, since this length ensures that the left Lagrangian moving boundary never gets too close to the mixing zone and that the reflected shock off the rigid wall on the right never approaches the mixing zone. In fact, by 819 µsec (which corresponds to the end of the experiment), the incident shock has still not reached the far wall nor has the left moving shock caught up to the Lagrangian boundary. Therefore, 70 cm is a conservative length to use for this problem.

Figure 1 shows a comparison of the mixing zone widths from a coarsely resolved KULL calculation (with 100 zones) to the experimental data. The experimental widths were obtained by examining Schlieren images, while the ones in the KULL calculation were calculated by interpolating the volume fraction profile for $SF₆$ between fraction values of .05 and .95. The agreement is quite good, although there is a slight overprediction at early times and a slight under-prediction at late times. The experimental data is only available between \sim 300 μ s and 750 μ s.

Figure 2 shows the same data as Figure 1, but also adds the mixing zone widths obtained by interpolating between the 99% and 1% values in volume fraction. It is evident that the value of the mixing zone width can vary significantly, depending on the cutoffs used to define it, especially if the volume fraction distribution has long tails. For this reason, we will use the 95% and 5% cutoffs to compare to the experimental data (and thus stay away from outliers) and fine-tune the model coefficients, but we will also show the 99% and 1% results on occasions where it will prove instructive.

Figure 3 shows a preliminary convergence study using meshes with 100, 200, and 400 zones, where we use the 95% and 5% volume fraction cutoffs. The results are somewhat mixed at early times, but at late times it appears as though we may be close to convergence, as the results for the 200 zone and 400 zone run are nearly identical. Figure 4 is identical to Figure 3, except now we use the 99% and 1% cutoffs. This figure is more consistent with what one would expect from a convergence study, namely that the widths decrease with increasing resolution (presumably, because the volume fraction profiles are becoming steeper under mesh refinement). The results in this figure indicate that 400 zones may not be sufficient.

Figure 5 shows the SF_6 volume fraction profiles at 819 µs. This figure helps explain why the results from the 100 zone calculation are so scattered. That is, there are only 4 mixed zones at late time in the coarsest calculation, and so we are more subject to interpolation problems. This figure also confirms our suspicions that the 400 zone calculation is not fully converged (at least, we cannot tell without performing higher resolution runs). It is also encouraging that the mixing region is better resolved as the zoning increases, since this means that at some point we should achieve a converged solution.

Running more than 400 zones on a single processor is starting to approach the diminishing returns limit, and so it is worth verifying that parallel runs give the same results as their serial counterparts. In this manner, we can continue to increase the resolution up to 1600 zones or higher. Figures 6 and 7 show pressure profiles and density profiles respectively at 819 µs. The serial run consisted of 100 zones on a single processor, while the parallel run used 2 processors with 1 processor having 49 onprocessor zones and the other having 51. The results confirm that identical results can be obtained for serial and parallel runs, and also that the python script that manipulates the array variables with various MPI calls is treating the data correctly in both cases.

Figure 8 shows the results of a more comprehensive convergence study where serial runs were performed up to 400 zones, a four processor run was used for the 800 zone calculation, and an eight processor run was employed for the 1600 zone calculation. This figure seems to indicate that "converged" results can be obtained with just 400 zones, since increasing the resolution does not significantly change the mix width. We would reach the same conclusion by examining Figure 9. Figure 10 shows the density

profiles at late time for the 3 highest resolution runs. It is interesting that if we focus on the mixing region (which at this time is approximately between 45 cm and 47 cm, it appears as though 800 zones are necessary for convergence. On the other hand, if we look in the vicinity of the shock front, then we could reasonably argue that we are converging much more slowly. Figure 11 confirms that 800 zones are sufficient to capture the turbulent mixing process for this problem.

Figure 12 shows the time evolution of the turbulent mixing zone for the 200 zone run in which we use a scalar zone centered Q (artificial viscosity) for one run and the CSW (Caramana-Shaskov-Whalen) edge centered Q [6-7] with (on) and without (off) the advection limiter for the other two runs. Since the artificial viscosity will only be felt at the shock front, and as there is no reshock in this problem, the results in Figure 12 should not be too surprising. That is, the mix widths are insensitive to the choice of artificial viscosity used in the KULL calculations. Other physics quantities, like density however, are sensitive, as Figure 13 makes evident. Here, the scalar Q and CSW Q with the limiter turned off give nearly identical results, while there are discernable differences between these runs and the one with the CSW Q with the limiter turned on. Basically, the limiter makes the shock front less diffusive.

Some comments are in order for describing the constant values used in the preceding calculations. The runs used to generate figures 1-13 used the following values for the EZturb model constants and switches:

 $\sigma_M = \sigma_\rho = .3$, $\sigma_U = .9$, $\sigma_K = 1$, $\sigma_e = 1.3$, $c_\mu = .09$, $c_{\epsilon 1} = 1.44$, $c_{\epsilon 2} = 1.92$, $c_{\epsilon 3} = 1.5$, $\delta_{iso} = 1$, $\delta_{aniso} = 0$, $\delta_{I,diss} = 1$

The initial value for the turbulent kinetic energy was chosen to be $1.44e7 \text{ cm}^2/\text{s}^2$, which is approximately equal to .12 times the shocked air speed squared. Since the initial amplitude was experimentally determined to be .24 cm, this value was used in conjunction with the kinetic energy to give an initial dissipation rate of 2.28e11 cm²/s³. Unfortunately, the only value that is "sacrosanct" is c_u . The other constants can be modified within reason. For example, in combustion applications with hydrocarbon gases, Prandtl number around .7 are usually observed. Self-similarity arguments also suggest that all of the σ 's, with the exception of σ_{ϵ} should be equal to each other. With these constraints in mind, as well as the fact that the mix widths change dramatically as we go from 100 zones to 400 zones, we can again attempt to match the data. Figure 14 shows the final result, with the settings now at:

 $\sigma_{\rm M} = \sigma_{\rm p} = \sigma_{\rm U} = \sigma_{\rm K} = .7$, $\sigma_{\rm e} = 1.3$, $\sigma_{\rm \mu} = .09$, $\sigma_{\rm e1} = 1.44$, $\sigma_{\rm e2} = 2.14$, $\sigma_{\rm e3} = 1.1$, $\delta_{\rm iso} = 1$, $\delta_{\rm aniso} =$ $0, \delta_{\text{I diss}} = 1.$

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Figure 1

Figure 2

Figure 3

Figure 4

Figure 5

Figure 6

Figure 7

Figure 8

Figure 9

Figure 10

Figure 11

Figure 12

Figure 13

Figure 14