



**SIMTRAN I—A Computer Code for the
Simultaneous Calculation of Oxygen
Distributions and Temperature Profiles in
Zircaloy During Exposure to High-Temperature
Oxidizing Environments**

S. Malang



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METALS AND CERAMICS DIVISION

SIMTRAN I - A COMPUTER CODE FOR THE SIMULTANEOUS CALCULATION OF OXYGEN
DISTRIBUTIONS AND TEMPERATURE PROFILES IN ZIRCALOY DURING
EXPOSURE TO HIGH-TEMPERATURE OXIDIZING ENVIRONMENTS

S. Malang

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FOREWORD

Postulated loss-of-coolant accidents (LOCA's) for light water reactors generally involve an excursion in temperature for parts of the reactor core in which the reaction of the Zircaloy fuel rods with the steam environment may become appreciable. The effects of the Zircaloy-steam reaction must be considered in the emergency core cooling system (ECCS) design because of their potential influence on both the thermal and mechanical behavior of the system. Thus, it is important to demonstrate a reliable method of evaluating and predicting quantitatively the extent of reaction during transient temperature exposures.

The Zirconium Metal-Water Oxidation Kinetics (ZWOK) program in the Metals and Ceramics Division of the Oak Ridge National Laboratory is generating kinetic data necessary for the above evaluation. An important part of this program is an investigation of the applicability of the models and mathematical treatments that can be used to describe the details of the reaction under transient temperature conditions. This is a complicated mathematical problem which can be handled satisfactorily only by computer techniques. While several analytical solutions and computer programs are available to examine simpler models of Zircaloy oxidation, the computer program, SIMTRAN I, described in this report, is a sophisticated calculation which yields a complete description of the oxygen distribution and temperature profiles for a variety of input or boundary conditions. The code is based on an ideal model which will eventually be tested by comparison of the theoretical and experimental results for a number of transient temperature excursions.

The code was written by Dr. Siegfried Malang, a visiting scientist on assignment to ORNL from Karlsruhe Nuclear Research Center. Since the editing and publication of this report has taken place since Dr. Malang's return to Germany, we apologize herewith - to Dr. Malang and to the readers - for any changes in meaning which have occurred as a result of the editing process. In addition, we would like to emphasize, as has been done in the body of the report, that while the program has survived numerous tests of its mechanical soundness, no serious testing has yet been accomplished that examines the individual or group accuracy of the input physical property, kinetic, or thermodynamic data for the Zircaloy-steam reaction. This aspect of the code's application will be reported at a later date when additional information to support a model verification will be available.

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ABSTRACT

SIMTRAN I is a Fortran IV computer program written for the IBM 360/91 system which solves SIMultaneously the TRANsport equations for both heat and mass flow for the one-dimensional, multiphase, moving-boundary, transient-temperature transport problem in a finite-geometry system defined by cylindrical coordinates. The code utilizes an ideal diffusion model which requires uniform layer growth of all phases and assumes the existence of thermodynamic equilibrium at all interfaces at all times. While SIMTRAN was constructed specifically for the consideration of oxidation phenomena during the reaction of Zircaloy fuel tubes with steam under high-temperature transient oxidation conditions, only minor changes are necessary to make it generally applicable to other materials and a number of oxidation, diffusion, and heat-transfer problems. A variety of boundary-condition options permit the mathematical simulation of a wide range of oxidation experiments.

The basic operational input to the code, which must include physical property, thermodynamic, and kinetic data over the desired temperature range, was selected from a variety of literature sources. Thus, while the results of the code yield acceptably accurate and self-consistent results in terms of the model and the mathematical operations, the user is cautioned to interpret the output results in terms of his confidence in his input information. The data presently incorporated into the code were assembled, at least in part, expeditiously and have not yet been subject to a critical evaluation either separately or as a whole (in terms of a model verification). Such information will be published at a later date.

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1. INTRODUCTION

The cladding of nuclear fuel rods in water cooled reactors is the first barrier against the release of fission products. Its integrity is especially important in a postulated Loss of Coolant Accident (LOCA) since in this case the second barrier - the pressure vessel and the primary coolant cycle - is partly open to the reactor containment.

The cladding material in all water-cooled power reactors is Zircaloy. This alloy has a good corrosion resistance against water at normal operating temperature. During a LOCA, however, the cladding temperature may rise to high levels. At such temperatures, Zircaloy will react vigorously with steam, and the resulting exothermal reaction can influence significantly the temperature attained during such an event.

The amount of oxidation during a LOCA also has an important influence on the mechanical strength of the clad and therefore its integrity. While the total weight gain due to the oxidation is a rough measure of the change in mechanical strength, a complete examination of the oxidation phenomena is necessary for a more detailed analysis of the behavior of the clad.

In addition to the oxide layer, there are two different metallic phases which exist for partially oxidized Zircaloy, depending on the temperature and the oxygen concentration. Since the ductility of the material is strongly influenced by the oxygen concentration, the distribution of the oxygen is generally a more important variable than the total oxygen content. This distribution can be calculated by application of the basic laws of diffusion to the three different layers in an oxidizing specimen.

A computer code based on a finite difference analysis has been developed which can simultaneously solve the oxygen diffusion and heat conduction equations for a material consisting of up to three different layers. A wide range of arbitrary boundary conditions for oxidation and heat transfer on both surfaces of a specimen can be used. The code has been designed primarily for the investigation of Zircaloy oxidation. It can be used, however, for a variety of oxidation, diffusion and/or heat transfer problems in other materials.

2. PROBLEM DEFINITION

The oxidation of Zircaloy at temperatures above the α/β transition range involves the dissolution of oxygen into the metal as well as the growth of layers of oxide and oxygen-stabilized alpha. The particular case of the reaction of steam with a Zircaloy fuel tube during a typical hypothetical LOCA is a complicated example of this general sort of behavior.

As part of an effort to develop a predictive capability by which to describe the extent of the Zircaloy-steam reaction during non-normal or accident conditions, the computer program SIMTRAK I has been written. The basic assumption invoked in obtaining solutions to the mass-transport equations is that thermodynamic equilibrium is maintained at all boundaries, regardless of their rate of movement or the rate of temperature change. Supersaturation in all phases is permissible when arrived at by temperature changes, and must be dissipated by diffusion and uniform phase growth rather than by precipitation. The growth of all phases is assumed to take place uniformly, in the manner envisioned when applying the ideal diffusion equations. In addition, it is assumed that each transport equation is completely characterized by a single kinetic parameter, although this parameter is generally a function of the particular phase, the temperature, and the oxygen concentration.

SIMTRAK I utilizes finite difference techniques to solve, in cylindrical coordinates, the one-dimensional, multiphase, moving boundary diffusion problem in a tube wall of finite thickness. Physical property data, as well as kinetic and thermodynamic parameters serve as the basic input to the code which, on the basis of the ideal model, can then examine simultaneously both the heat and mass transport processes that occur during a given reaction. Both isothermal and transient temperature oxidation can be studied as well as oxidation in a particular reaction environment where self-heating of the specimen might take place. In addition, the high degree of flexibility in defining the boundary conditions in this program permits the modeling of a large number of useful reaction sequences.

3. MODEL, METHODS, AND ASSUMPTIONS

A finite difference approach is used for the calculation of both temperature profiles and oxygen distributions. The general finite difference methodology for diffusion in a system without moving boundaries is well known and will, therefore, be described only very briefly. More emphasis will be placed on the description of the specific method used here to deal with the problem of the moving boundaries.

3.1 General Method for the Calculation of Temperature Profiles and Oxygen Distributions

The method will be explained for a flat wall in order to keep the description as simple as possible. The code itself uses cylindrical coordinates.

The basic equations for one dimensional conduction and diffusion in a flat wall are

$$\frac{\partial T}{\partial \tau} = \alpha \cdot \frac{\partial^2 T}{\partial x^2} \quad (1)$$

$$\frac{\partial C}{\partial \tau} = D \cdot \frac{\partial^2 C}{\partial x^2} \quad (1a)$$

where

x [cm] = distance

τ [sec] = time

T [°C] = temperature

α [$\frac{\text{cm}^2}{\text{sec}}$] = thermal diffusivity

C [$\frac{\text{gram}}{\text{cm}^3}$] = concentration
(i.e., oxygen in Zircaloy)

D [$\frac{\text{cm}^2}{\text{sec}}$] = oxygen diffusion coefficient

The use of a finite difference method defines the wall as being divided into a number of nodes in which all the mass is assumed to be concentrated. These nodes are connected by "conductors" which "conduct" heat and oxygen. The differential equations (1) and (1a) are converted to the following difference equations:

$$\underbrace{\frac{T_n^* - T_n}{\Delta\tau}} (\rho \cdot c \cdot v)_n = \underbrace{L_{t,n,n-1} (T_{n-1} - T_n)}_{\text{net heat transport}} + \underbrace{L_{t,n,n+1} (T_{n+1} - T_n)}_{\text{net heat transport}} + \underbrace{q}_{\text{heat generation in node n}} \quad (2)$$

change in stored heat

net heat transport

heat generation in node n

$$\underbrace{\frac{C_n^* - C_n}{\Delta\tau}} \cdot v_n = \underbrace{L_{c,n,n-1} (C_{n-1} - C_n)}_{\text{net diffusion}} + \underbrace{L_{c,n,n+1} (C_{n+1} - C_n)}_{\text{net diffusion}} \quad (2a)$$

change in oxygen content

net diffusion

Equations (2) and (2a) show the heat and mass transport balances for the node n. T_n and C_n are the mean temperature and concentration values at the time τ ; T_n^* and C_n^* are the corresponding values at the time $\tau + \Delta\tau$. The meaning of the other symbols is:

$$\rho \left[\frac{\text{Gram}}{\text{cm}^3} \right] = \text{density}$$

$$c \left[\frac{\text{Ws}}{\text{gram}^\circ\text{K}} \right] = \text{specific heat}$$

$$v \left[\text{cm}^3 \right] = \text{volume}$$

$$L_t \left[\frac{\text{W}}{\text{K}} \right] = \text{conductance, thermal conductor}$$

$$L_c \left[\frac{\text{cm}^3}{\text{sec}} \right] = \text{conductance, oxygen 'conductor'}$$

$$q \left[\text{w} \right] = \text{heat generated in node during } \Delta\tau.$$

L_t and L_c can be determined with the equations

$$L_t = K \cdot \frac{A}{X} \quad (3)$$

$$L_c = D \cdot \frac{A}{X} \quad (3a)$$

where X [cm] is the distance between the two nodes and A the cross-sectional area [cm²] of the conductor. K [$\frac{W}{cm \cdot K}$] is the thermal conductivity and D [$\frac{cm^2}{sec}$] is the oxygen diffusion coefficient. "A" is usually chosen to be 1 cm² for convenience. The equations (2) and (2a) have to be solved for each node. The sets of solutions comprise the temperature profiles and oxygen distributions as functions of time. Arbitrary boundary conditions as well as temperature dependent and concentration dependent material properties can be used with this method.

As part of the basis for the temperature calculation, it is assumed that a reaction heat (specified as $34330 \frac{Ws}{gram \text{ oxygen}}$) is generated at the oxide- α interface. The heat which is necessary to split steam into O and H₂ at the gas-oxide interface must also be accounted for. The fraction of this energy supplied by the specimen is specified as an input.

3.2 Treatment of the Moving Boundaries

The basic assumption of the entire method is that the oxygen concentration on both sides of an interface between two phases is always the equilibrium concentration. Such an assumption is almost universal in isothermal, diffusion-controlled oxidation processes, but it is difficult to judge how accurate it is in transient temperature cases. Therefore, a particularly important check on the validity of the code will be its ability to predict the results of transient temperature oxidation experiments after the adjustment of the kinetic input parameters determined on the basis of the results of isothermal experiments. The treatment is presented without explicit consideration of density changes in the phases during oxidation. The method chosen to account for this effect is discussed in par. 3.7.

Two different methods are used for the treatment of the moving boundaries, depending upon the thicknesses of the oxide and alpha Zircaloy layers.

3.21 Oxide Layer Less Than 4 μm Thick

To avoid excessive computing time, the mesh sizes for the main diffusion calculations are chosen in such a way that the oxide layer must be at least 4 μm and the alpha layer at least 6 μm thick in order for the calculations to be made. To enable the code to describe the growth of very thin layers, a separate simplified method was developed that utilizes only two nodes in each of the oxide and alpha layers. This stipulation results in the assignment of linear concentration gradients to these thin growing layers. This method will be described with the help of Fig. 1 which shows the oxygen concentration profile near the surface. Only a few nodes in the beta layer are shown, but the code calculates over the entire wall.

The three oxygen fluxes, FLUX O, A, and B, are each kept constant during one time step $\Delta\tau$. The movement of the interfaces after each time step is calculated in the following way.

$$S_0^* - S_0 = \frac{(\text{FLUX O} - \text{FLUX A}) \cdot \Delta\tau + S_0 \cdot (\bar{C}_O - \bar{C}_A^*)}{\bar{C}_O^* - \bar{C}_A} \quad (4)$$

$$S_A^* - S_A = \frac{(\text{FLUX A} - \text{FLUX B}) \cdot \Delta\tau + S_A (\bar{C}_A - \bar{C}_A^*)}{\bar{C}_A^* - \bar{C}_B} \quad (5)$$

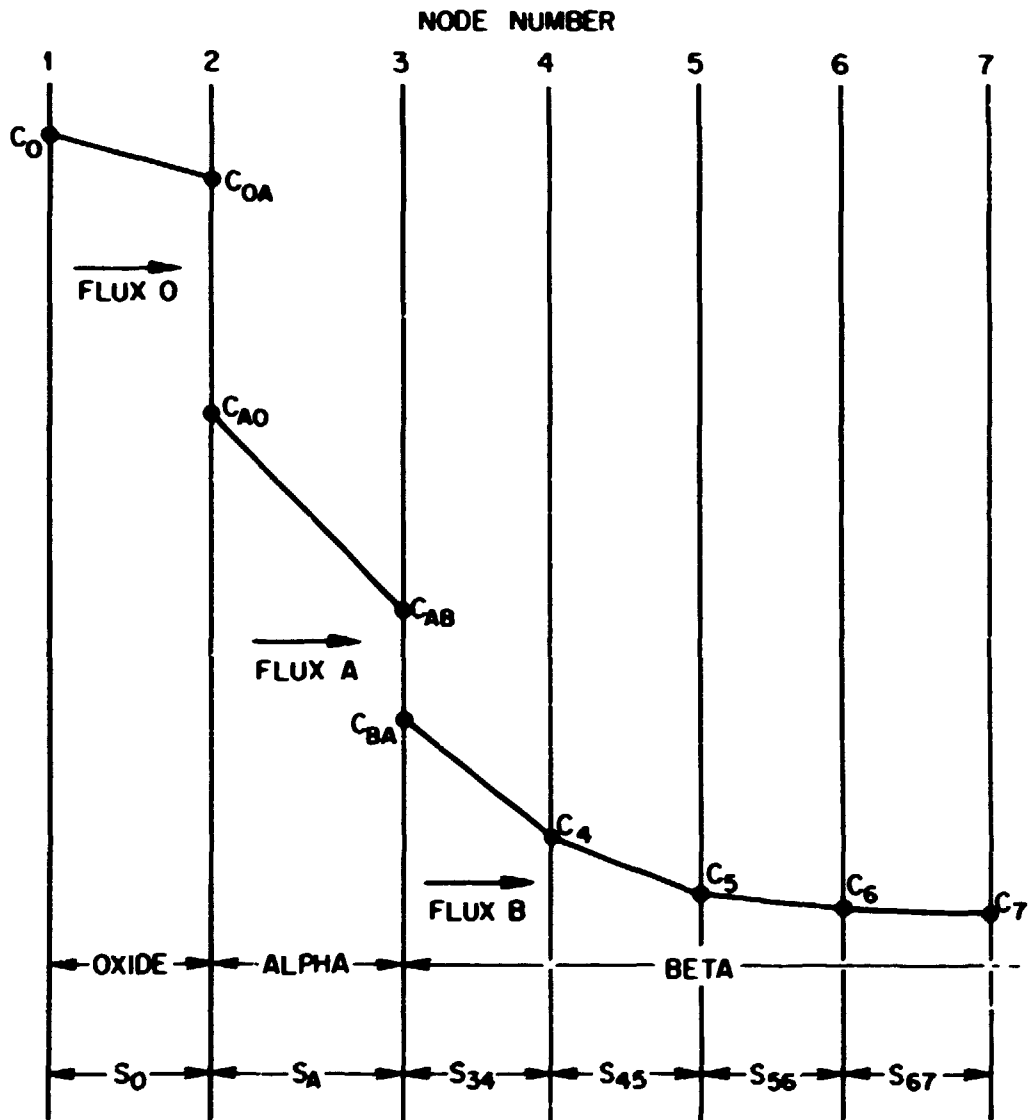


Fig. 1. Model for the treatment of moving boundaries for thin layers.

The meaning of the symbols is: (see Fig. 1)

Δt [sec] time step

$$\text{FLUX O} = D_O \frac{C_O - C_{OA}}{S_O} \quad (6)$$

$$\text{FLUX A} = D_A \frac{C_{AO} - C_{AB}}{S_A} \quad (7) \text{ oxygen fluxes}$$

$$\text{FLUX B} = D_B \frac{C_{BA} - C_4}{S_{34}} \quad (8)$$

$$\bar{C}_O = \frac{C_O + C_{OA}}{2} \quad \left[\frac{\text{gram}}{\text{cm}^3} \right] \quad \text{Average oxygen concentration in oxide.}$$

$$\bar{C}_A = \frac{C_{AO} + C_{AB}}{2} \quad \left[\frac{\text{gram}}{\text{cm}^3} \right] \quad \text{Average oxygen concentration in alpha-Zircaloy.}$$

$$\bar{C}_B = \frac{C_{BA} + C_4}{2} \quad \left[\frac{\text{gram}}{\text{cm}^3} \right] \quad \text{Average oxygen concentration in beta Zircaloy between nodes 3 and 4.}$$

$$\begin{array}{l} C_{OA} \\ C_{AO} \\ C_{AB} \\ C_{BA} \\ C_4 \end{array} \quad \left[\frac{\text{gram}}{\text{cm}^3} \right] \quad \text{Concentrations at the various interfaces; see Fig. 1.}$$

$$\bar{C}_O^*, \bar{C}_A^* \quad \left[\frac{\text{gram}}{\text{cm}^3} \right] \quad \text{Concentrations after time step } \Delta t. \text{ (Can be different from } \bar{C}_O, \bar{C}_A \text{ if temperature changed during time step.)}$$

$$S_O, S_A \quad [\text{cm}] \quad \text{Thicknesses of oxide and alpha layers at start of time step.}$$

$$S_O^*, S_A^* \quad [\text{cm}] \quad \text{Thicknesses of oxide and alpha layers at end of time step.}$$

The concentration in the beta phase is calculated by using the general method described in section 3.1.

3.22 General Treatment of the Moving Boundaries

The concentration gradients and interface movement for oxide and alpha Zircaloy are computed by using the method described in section 3.21 for layer thicknesses up to 4 and 6 μm , respectively. For thicker layers, a different method is used which, in general, makes use of at least four nodes in each phase. These methods shall be described focusing on the profiles at the oxide/alpha interface as illustrated in Fig. 2.

The oxygen fluxes, FLUX OA and AO, and the concentrations are kept constant during the time step $\Delta\tau$. After this time step, the movement of the interface is calculated from the following equations:

$$S_{O1} \cdot \frac{C_{O1} + C_{OA}}{2} + S_{Al} \cdot \frac{C_{AO} + C_{Al}}{2} + (\text{FLUX OA} - \text{FLUX AO}) \cdot \Delta\tau$$

$$= S_{O1}^* \cdot \frac{C_{O1}^* + C_{OA}^*}{2} + S_{Al}^* \cdot \frac{C_{AO}^* + C_{Al}^*}{2} \quad (9)$$

$$S_{O1} + S_{Al} = S_{O1}^* + S_{Al}^* \quad (9a)$$

For a flat wall the oxygen fluxes would be:

$$\text{FLUX OA} = D_O \frac{C_{O1} - C_{OA}}{S_{O1}} \quad (10)$$

$$\text{FLUX AO} = D_A \frac{C_{AO} - C_{Al}}{S_{Al}} \quad (11)$$

The symbols are similar to those used in par. 3.21, with reference to Fig. 2. The code solves the equations (9) - (11) for cylindrical coordinates. The movement of the alpha-beta interface is treated in an identical manner.

The concentrations in the nodes inside the three layers are all calculated according to the methods outlined in section 3.1. The possible boundary conditions at the surfaces of the wall are described in the next section.

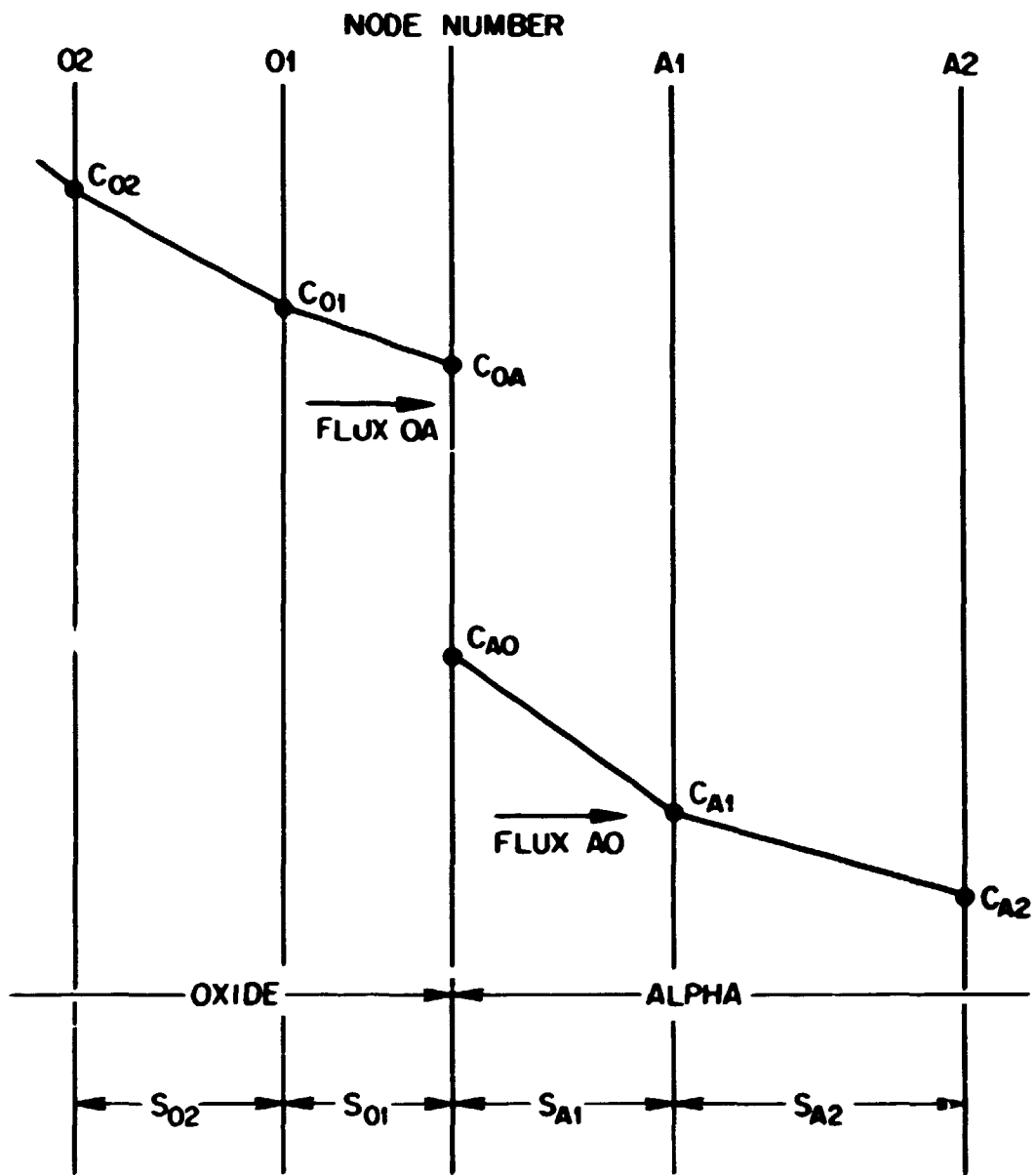


Fig. 2. Model for the general treatment of moving boundaries.

3.3 Boundary Conditions at the Two Surfaces of the Wall

The code allows for oxidation and/or heat transfer at the inner surface, at the outer surface, or at both surfaces of a hollow cylinder. All boundary conditions can be time dependent.

3.31 Boundary Conditions in Regard to Temperature Profile Calculations

Three kinds of heat transfer associated with each surface can be specified:

- a) Convection, determined with h , T_{cool}
- b) Radiation, determined with ϵ , T_{wall}

where T_{cool} is the temperature of the gas stream in contact with each surface; T_{wall} is the temperature of the surroundings with which the specimen exchanges heat by radiation; h is the convective heat transfer coefficient; and ϵ is the Stefan-Boltzmann constant.

- c) Fixed heat flux (independent of specimen temperature or heat transfer by convection or radiation).

3.32 Boundary Conditions in Regard to Concentration Profile Calculations

An upper limit for the oxygen flux available to either surface can be specified. As long as the actual oxygen flux, determined by the diffusion constant and the concentration gradient, is smaller than this limit, stoichiometric oxide at the surface is assumed. Otherwise the concentration at the surface node is calculated with the equation:

$$C_1 = C_n + Q_{\text{limit}} \cdot (r_1 - r_n)/D \quad (12)$$

where

- | | | |
|--|---|---|
| $C_1 \left[\frac{\text{gram}}{\text{cm}^3} \right]$ | = | oxygen concentration at the surface. |
| $C_n \left[\frac{\text{gram}}{\text{cm}^3} \right]$ | = | oxygen concentration at the next node. |
| $r_1 - r_n \left[\text{cm} \right]$ | = | distance between the two nodes. |
| $Q_{\text{limit}} \left[\frac{\text{gram}}{\text{cm}^2 \cdot \text{sec}} \right]$ | = | upper limit for oxygen flux to the surface. |
| $D \left[\frac{\text{cm}^2}{\text{sec}} \right]$ | = | diffusion coefficient. |

The purpose of the variable O_{limit} is to allow the effect of gas phase control of the oxidation rate, or "steam starvation," to be observed. In the present version of the code, O_{limit} is an input which can be time dependent. If this variable (for either side) is specified in the code as uniquely zero, then no oxidation takes place on that side. If intermittent oxidation (i.e. oxidation-annealing steps or tube-burst simulation) is desired, then the oxygen flux limit for the periods when no oxidation is taking place is given by some small number greater than zero, such as 1×10^{-20} .

3.4 Selection of Mesh Sizes

It can be shown that the stable time step for the integration (see section 3.5) is proportional to the square of the mesh size. Since the number of nodes increases linearly with decreasing mesh size, the computing time increases approximately with $(1/\text{mesh size})^3$. Therefore, it is important that small mesh sizes be used only at the places and times when it is really necessary. For example, for temperature calculations a larger mesh size should be used in the metal than in the oxide since the thermal conductivity in the metal is much larger and, therefore, the temperature gradients much smaller.

Similarly for diffusion calculations, a larger mesh size can be used in the beta phase than in the alpha phase or the oxide. In addition, it would be desirable to keep the number of nodes in the oxide and alpha layer approximately constant, independent of the layer thickness. For all these reasons, up to seven different mesh sizes may be used to complete a typical calculation. This means that the mesh size can and will vary as a function of purpose (temperature or diffusion calculation), phase (oxide, alpha, or beta), and layer thickness (and, therefore, time). To determine the smallest mesh size, DR, the largest integer M for the equation

$$DR = \frac{\text{wall thickness}}{M^2} \geq 1 \text{ } \mu\text{m} \quad (13)$$

is calculated. This basic (minimum) mesh size is used for diffusion calculations in the thinnest oxide and alpha phases only. For other purposes, mesh sizes determined by multiplying DR by 2, 4, 8, 16, 32, or 64 are used. The particular mesh sizes for specific uses can be seen in Table 1. It should be mentioned, however, that the interfaces between the different phases do not have to be exactly at the location of a node but may be located between them.

For the selection of the mesh size for diffusion calculations, the following guidelines are used.

- a) mesh size in alpha = mesh size in oxide
- b) mesh size in beta = 2 x mesh size in alpha for the 10 meshes adjacent to the α/β interface, otherwise 64 DR.
- c) oxide layer is divided into at least 2 meshes
- d) alpha layer is divided into at least 3 meshes
- e) not more than 8 meshes in alpha layer if this is not a contradiction to c), given condition a)
- f) not more than 8 meshes in oxide layer if this is not a contradiction to d), given condition a).

Using these guidelines, the mesh sizes can increase or decrease during the computation, depending on which direction the interfaces are moving, in order to create a balance between accuracy and computing time.

3.5 Integration Method

In cases with fast temperature changes, the heat conduction equation (2) and the diffusion equation (2a) have to be solved simultaneously since the diffusion constants and equilibrium oxygen concentrations, especially, are strongly temperature dependent. The most simple method to do this is to use an explicit integration scheme. An explicit method, however, has the disadvantage of having a very small stable time step, which can lead to a very long computing time for many useful types of cases. To keep the option for the implementation of an implicit method open, the concentration and temperature integrations are performed in

Table 1. Mesh sizes utilized in computations

		MESH SIZE						
		1 DR	2 DR	4 DR	8 DR	16 DR	32 DR	64 DR
TEMPERATURE CALCULATIONS	ALPHA BETA							Y
	OXIDE							
DIFFUSION CALCULATIONS	ALPHA OXIDE	←				→		
	BETA		←					→

separate subroutines. An alternate integration scheme can, therefore, be added without too many problems. As a first approach, a compromise was made by using an explicit integration utilizing up to four different time steps.

The appropriate stability criteria are given by the equations:

$$\Delta\tau_a \leq \frac{(c \cdot s \cdot v)_n}{\tau_{t,n,n-1} + \tau_{t,n,n+1}} \quad (14)$$

$$\Delta\tau_b \leq \frac{v_n}{c_{n,n-1} + c_{n,n+1}} \quad (14a)$$

where

$\Delta\tau_a$ = stable time step for the finite difference equation for the temperature calculations

$\Delta\tau_b$ = stable time step for the finite difference equation for the concentration calculations.

The meaning of the symbols is the same as in Eq. (2) and (2a).

In addition, use is made of $\Delta\tau_c$, a maximal time increment during which all boundaries and material properties for temperature calculations are kept constant, and $\Delta\tau_d$, a maximal time increment during which all boundaries and material properties for concentration calculations are kept constant.

Equations (14) and (14a) have to be applied to each node, and the smallest of the two stable time steps, $\Delta\tau_a$ and $\Delta\tau_b$, is used. It can be seen that $\Delta\tau_a$ and $\Delta\tau_b$ depend only on the mesh size and the values of the thermal conductivity or diffusion constant. If $\Delta\tau_a$ or $\Delta\tau_b$ is small, then this small step has to be used even for very slow transients to insure stability of the finite difference solutions. However, in this case it is practical to change the model so that the much larger time increments $\Delta\tau_c$ and $\Delta\tau_d$ can be used. Therefore, provisions are made in the code so that a number of $\Delta\tau_a$ (stable) steps can be performed between a single $\Delta\tau_c$ step; similar provisions are made for $\Delta\tau_b$ and $\Delta\tau_d$. The calculations which have to be repeated for each step $\Delta\tau_a$ and $\Delta\tau_b$ are kept as simple

as possible. The test runs showed that this approach together with the automatic time step control (see section 3.4) leads to a reasonable computing time for diffusion calculations for both high and low oxidation temperatures. Only if a detailed temperature calculation is desired for cases with low oxidation temperatures will the computing time be excessively long. A "lumped" (see par. 5.1) temperature calculation would be more appropriate for those cases. A rough rule of thumb for the computing time in reasonable cases is, for an IBM 360/1, that about 1.5 min is required for each 100 μ m movement of the α/β interface. Due to the automatic time step control, the computing time is not highly dependent on oxidation temperature and layer thickness.

3.4 Time Step Control

The optimal time step for temperature and concentration calculations varies over a wide range. This is due to the strong temperature dependence of the material properties, especially the diffusion constants. In addition, the optimal time step depends on the mesh size which varies with layer thickness. Therefore, the time step may vary from 10^{-6} sec to a few seconds in a single experiment.

It would be very difficult if not impossible to find manually a satisfying compromise between precision and computing time. Therefore, an automatic time step control has been chosen. Using this feature, the user has only to specify the time step for printing out the results. The code uses the four different time steps mentioned in section 3.5 for calculation. There are different levels of control. The first level assures stable time steps for temperature and concentration calculations. These time steps are determined with Eq. (14) and (14a), and the values are never exceeded. They are used for the integration in the explicit method. The next level controls the time steps during which all boundary conditions and material properties are kept constant. These steps can be specified by the user, but they are checked by the code itself. The code calculates upper limits which are actually used if the step specified by the user is larger than the calculated upper limit or if the step size is not

specified at all. These upper limits are calculated so that the following conditions are not exceeded during the time step:

1. For the temperature profile calculations, the temperature at the wall surface does not change by more than 1°C.
2. For the concentration profile calculations,
 - (a) the oxygen gain at one surface is limited to the amount which is necessary for the oxidation of $2 \cdot 10^{-6}$ cm Zircaloy to stoichiometric oxide;
 - (b) the oxide - α interface shall not move more than $2 \cdot 10^{-6}$ cm; and
 - (c) the γ/α interface shall not move more than $5 \cdot 10^{-6}$ cm.

The values specified above are not inputs to the code. A user, however, can change them easily if desired. They are only the result of a first approach and could be optimized later in a sensitivity analysis. It is not recommended, however, that the user generally attempt to specify the time steps as an input.

3.7 Volume Changes Associated with Oxidation

It is assumed that the entire volume increase associated with the oxidation of Zircaloy to Zircaloy oxide takes place in one dimension. In all the calculations, however, the properties of a fictive material are used instead of those of the "real" oxide in order to facilitate the keeping of the mathematical origin ($x = 0$) at the original wall surface. Only for the output of the program is the increase in wall thickness due to oxidation calculated. To determine the properties of this fictive material, the following conversion factor is calculated:

$$\text{FICFAC} = \frac{\text{DENZIR}}{\text{DENZO} - \text{OSTOCH}} \left[\frac{\text{cm}^3 \text{ oxide}}{\text{cm}^3 \text{ metal}} \right] \text{ volume ratio} \quad (15)$$

where

$$\text{DENZIR} \left[\frac{\text{gram}}{\text{cm}^3} \right] = \text{density of Zircaloy}$$

$$\text{DENZRO} \left[\frac{\text{gram}}{\text{cm}^3} \right] = \text{density of ZrO}_2$$

$$\text{OSTOCH} \left[\frac{\text{gram}}{\text{cm}^3} \right] = \text{oxygen density in stoichiometric ZrO}_2$$

The conversions between the real values of the properties in the oxide and the fictive values (written with +) are:

$$\begin{aligned} S^+ &= S/\text{FICFAC} && \text{layer thickness} \\ D^+ &= D/\text{FICFAC}^2 && \text{diffusion constant} \\ C^+ &= C \cdot \text{FICFAC} && \text{oxygen concentration} \\ (C_p \cdot \rho)^+ &= C_p \cdot \rho_{\text{ZrO}_2} \cdot \text{FICFAC} && \text{heat capacity} \\ K^+ &= K/\text{FICFAC} && \text{thermal conductivity} \end{aligned}$$

The volume change associated with the transition from β -Zircaloy to α is neglected as well as the small effect of oxygen concentration on the density in all the phases.

4. GENERAL FEATURES OF THE CODE

The features of the code development can be summarized as follows:

1. The code permits simultaneous determination of the temperature and oxygen profiles for a variety of typical oxidation experiments.
2. All material properties input to the program are located in separate subroutines so that changes can be made easily.
3. All physical, thermodynamic and kinetic variables are input to the program as temperature dependent functions.

4. Diffusion constants may be designated as concentration dependent, if desired.

5. It is possible to specify an upper limit for the oxygen flux into the wall, which permits the effects of gas-phase control of the kinetics to be examined.

6. Oxidation and heat transfer may occur at either or both free surfaces of the tube.

7. All boundary conditions may be time dependent.

8. Options are included for performing several simpler oxidation calculations such as total oxygen calculations based on the data of Baker-Just, Houson, or Lemmon.

9. Options are provided whereby either a complete temperature profile may be calculated, or the temperature calculated on the basis of no temperature gradient (Lumped). The latter is useful when gradients are expected to be small, and it results in an appreciable saving in computation time.

Figure 3 shows the flow chart for the code. The general outline and the calling sequence for the subroutines are shown. In the following sections, the purpose of each subroutine is described briefly.

4.1 Main Program, SIMTRAN

This is a short and simple program which calls the different subroutines where the various computations are accomplished. In addition, the time step control and selection described in section 3.6 is performed here.

4.2 Subroutines INPUT and INDATA

These routines read all the input data and print them out. No elaborate calculations are made.

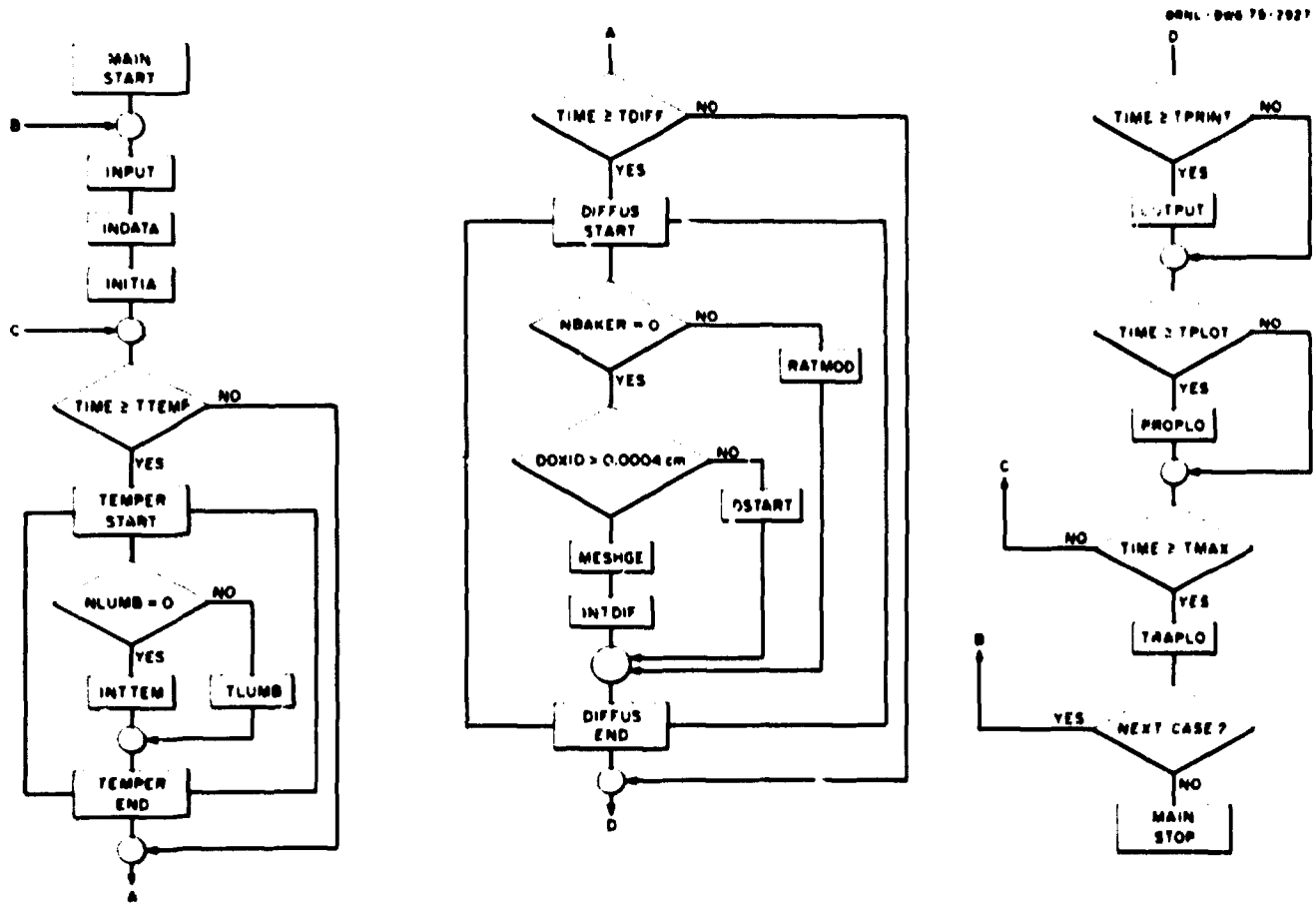


Fig. 3. Flow chart for SIMTRAN I

4.3 Subroutine INITIA

In this routine, initial values are assigned to a number of boundary condition variables.

4.4 Subroutines TEMPER, TLUMB, and INTTEM

In TEMPER, the temperature calculation is prepared. If the option for a lumped temperature calculation is used, the subroutine TLUMB is called and the temperature calculated there. The subroutine INTTEM is called for the calculation of the temperature distribution across the wall.

4.5 Subroutines DIFFUS, DSTART, MESHGE, INTDIP, and RATMOD

These are the largest and most complicated subroutines of the code. They calculate the oxygen distribution throughout the wall. The controlling routine is DIFFUS. Depending upon the layer thickness and other specified options, the other subroutines are called. DSTART performs the complete diffusion calculation for thin oxide and ν layers. For thicker layers the calculation is prepared in DIFFUS and MESHGE, and the integrations to provide values of total oxygen uptake are performed in INTDIP. RATMOD is used for the total-oxygen calculations based on the Baker-Just, Hobson or Lemmon data. With these equations it is assumed that all the oxygen consumed forms stoichiometric ZrO_2 .

4.6 Subroutines OUTPUT and PREPAR

OUTPUT prints out the results in specified time steps. It calls PREPAR to calculate the oxygen content in each phase and to prepare the variables for plotting.

4.7 Subroutines PROPLO and TRAPLO

PROPLO is a cathode ray tube (VIDEO) plotting routine which plots the oxygen profile in the wall in specified time steps. The time steps

are chosen as multiples of the output time step. The concentration can be plotted in two different scales which are selected by the user. With one scale the profiles in oxide, α - and β -Zircaloy are plotted; with the other, only the α and β profiles are plotted. The user can select one of them or both.

TRAPLO is a pen-and-ink (CALCOMP) plotting routine which plots up to 25 output variables as functions of time or square root of time. Both routines use the standard plotting package of the ORNL-computers which is described in Appendix A.

4.2 Functions for Material Properties

The code must contain a set of functions for the calculation of the material properties. No claim is made that the equations presently used for these functions are the best ones. They are rather considered to be reasonable values which may be used for testing purposes.

For every case, a table with the material properties in the range from 750°C to 1500°C (1382-2732°F) is calculated and printed with the subroutine MATMAP. The subroutines which furnish these data to the computational routines are:

1. INTFAC: Calculates equilibrium oxygen concentrations at all phase boundaries.
2. DIFCON: Calculates oxygen diffusion constants for all phases.
3. CONDOC: Calculates thermal conductivity for all phases.
4. SPEC: Calculates heat capacity (product of specific heat and density) for all phases. This subroutine is presently utilized to account for the heat of the α - β transformation by appropriately modifying the specific heat input.

The temperature application limit of these functions is presently arbitrarily restricted to a maximum of 1550°C (3362°F) (melting point of Zircaloy). A lower limit of 850°C (1562°F) is arbitrarily set in INTFAC for the solubility data calculations. Except for specific heat values,

these temperature limits are used for the calculation of the material properties, and arbitrary constant values are applied outside these limits. It should be realized, of course, that the oxidation model applied by the program is not valid outside the temperature range approximately 850-1500°C (1562-2732°F) in any event.

5. DESCRIPTION OF THE INPUT AND OUTPUT DATA

All input and output data are listed in Appendix B and C. In addition, three sample problems are given in Appendix D. Therefore, the description here is restricted to the use of the major options.

5.1 Temperature Calculations

The particular option for this calculation is specified with the variable NLUMB (card 4, field 1-10). There are three different options:

a) NLUMB = 0

The complete temperature distribution across the wall is calculated. This calculation increases the computing time considerably. In cases where the temperature gradients are expected to be small, options (b) or (c) can be substituted with little loss in definition.

b) NLUMB = 1

The entire wall is treated as one node only (referred to as a "lumped" calculation). The temperature is calculated as a function of heat transfer at the two surfaces and the heat generation associated with the oxidation. The nature of the heat transfer is specified in data cards 5 and 6. Every combination of oxidation, convective heat transfer, radiation, and fixed heat flux can be specified for each surface.

c) NLUMB = 2

With this option, the wall temperature is identical with the variable TSTEAM(1) (card 5, field 21-30). No heat transfer coefficients have to be specified. If TSTEAM(1) is zero, TSTEAM(2) (card 6, field 21-30) is used instead.

5.2 Concentration Calculations

The surface where oxidation occurs is specified with the variables HDIFF(1) and HDIFF(2) (card 5 and 6, field 1-10) which set the maximum oxygen flux available at each surface. If there is oxidation on one or both surfaces, the corresponding HDIFF has to be greater than zero. After oxidation has occurred on a given surface, HDIFF can then be made arbitrarily small (but not zero) for the remainder of the transient or for a part of it. Thus, intermittent oxidation - annealing steps can be considered.

If the oxygen distribution in the wall is to be calculated, the variable NBAKER (card 4, field 11-20) has to be zero. For:

a) $NBAKER = 0$,

the oxygen concentration profile is calculated as a function of time, starting with a constant concentration across the wall, given by CSTART (card 11, field 11-20).

b) $NBAKER > 0$,

only the total oxygen gain is calculated. It is assumed in this case that all the oxygen forms stoichiometric oxide. There are no provisions for limiting the oxygen supply. Specifically, for:

b1) $NBAKER = 1$, the Baker-Just equation is used.

b2) $NBAKER = 2$, the Hobson equation is used.

b3) $NBAKER = 3$, the Lemmon equation is used.

6. CONCLUSION AND OUTLOOK

A number of cases with a variety of boundary conditions have been considered with the code for testing purposes. Preliminary results have shown excellent mechanical operation and self-consistency in the calculations. Further testing and model verification is in progress.

So far, it has been shown that in nearly all practical cases, a lumped (single-node) temperature calculation is adequate; this leads to

a considerable saving in computer time compared to the more detailed temperature calculation. Generally, the maximum temperature difference in a specimen exceeds one to two degrees only in cases where comparatively thick oxide layers exist and where a large heat flux through the wall is specified by the experimental conditions.

No attempt has been made yet to select or to adjust the equations for the materials properties in order to get the best possible agreement between calculation and experiment. To aid in this purpose, a specialized version of the code will be developed which utilizes experimental data from isothermal oxidation rate measurements as input and selects by an optimization scheme the "best" diffusion constants and equilibrium concentrations for all three phases as functions of temperature. We consider such an optimization step to be of great importance, and all users of the code are strongly advised to keep this fact in mind. The various material parameters contained in the code were selected from a variety of literature sources, and at this time we can offer no assurances as to their correctness despite the fair agreement we have obtained between calculated and early experimental results. The final verification of SIMTRAN I awaits the completion of the experimental phase of our program, and not until that time will we be able to comment on the applicability of the code to the steam-Zircaloy reaction over a wide temperature range or on the validity of the material parameters presently incorporated in the code.

7

APPENDIX A

DESCRIPTION OF THE PLOTTING ROUTINES*

A1. Calcomp Pen and Ink Plotter Subroutines

The Calcomp tape transport accepts a seven-track magnetic tape written on the IBM/360 computers in a special format and uses data from this tape to drive the pen and ink plotters. The basic plotting package may be called by FORTRAN programs. A description of the subroutines and their calling sequences follows. The basic plotting package performs all necessary manipulations to generate the tape for plotting.

The package computes the incremental steps necessary to move the plotter from its current (X,Y) position to the (X,Y) position given in the calling sequence. The data generated are stored in an array and written onto magnetic tape each time the array is filled or when an end-of-graph call is given. Sequential graph addresses are generated for each graph written, and the graph address is displayed to the Calcomp operator as plotting progresses.

Subroutine PLOTS has two entry points. The first entry, PLOTS, is used to initialize the routine by transmitting parameters indicating the location of a storage area available to the routine and the length of the storage area. The second entry, PLOT, is used to convey coordinate data to be converted into incremental plotter commands.

Initialization Entry - CALL PLOTS (A, LENGTH)

A is the first location of a storage area which may be used by the routine for accumulating data to be written on tape. Normally, an array is set aside for this purpose.

LENGTH is an integer such that $47 \leq \text{LENGTH} \leq 8191$ which specifies the number of consecutive four-byte locations beginning with location A available to the routine. If A is an array, then LENGTH is the dimension of the array. For plotting efficiency, the value of LENGTH should be

*Taken from "Programmer's Notebook," Computer Science Division, Oak Ridge National Laboratory, Section 13, (June 1975).

between 3000 and 5000. The programmer must not use that portion of storage from location A through location A (LENGTH) at any time between the initialization of the package and the final use of the routine.

Plotting Entry - CALL PLOT (X,Y,I)

This call generates the necessary plotter commands to move the pen in the nearest approximation of a straight line from the current (X,Y) position to the (X,Y) given in the calling sequence. The arguments are as follows.

X is the abscissa in inches expressed in floating point.

Y is the ordinate in inches expressed in floating point.

I is an integer which specifies whether or not the pen is to contact the paper while moving to the new (X,Y) position. The sign of I specifies either a continuation of the current graph ($I \geq 0$) or an end-of-graph call ($I < 0$).

If $|I| \geq 3$, the pen will be lifted prior to execution of the movement to given (X,Y) position; if $|I| = 2$, the pen will be lowered and a straight line drawn to the given (X,Y) position; and if $|I| = 0$ or 1, the pen will not be altered. If $I < 0$, the command will be interpreted as an end-of-graph call, and following movement to the given (X,Y) position, the X reference point will be set to 0 to establish a new origin for the following graphs. Note also that $|I|$ will determine whether the pen is lifted on this final call for each graph. The end-of-graph call also causes any data remaining in the storage area to be written out and the sequential graph number to be incremented. PLOT keeps track of the current status of the pen so that redundant pen commands are not generated.

Subroutine SYMBOL. - This routine provides the programmer with the ability to draw alphanumeric characters. It may be used for labeling, annotation, data point plotting, legends, etc. It allows the programmer to choose the size of the characters and the orientation to suit himself. One hundred twenty-seven alphanumeric characters are available in the SYMBOL routine.

The calling sequences and arguments are given below.

Entry - SYMBOL. - Two functions are served by this entry point. Although the calling sequences are very similar, each will be described individually to avoid confusion. The normal entry is used for titles, identification, etc. The calling sequence is

CALL SYMBOL (X, Y, H, BCD, THETA, N),

where

- X is the abscissa of the left edge of the first character to be drawn.
- Y is the ordinate of the lower edge of the first character to be drawn.
- H is the height, in inches, of the characters to be drawn and $H \geq 0.035$. Best results will be obtained if H is an integral multiple of 0.035; e.g., 0.035, 0.07, 0.105, 0.14 The width of a character is four-sevenths of the height.
- BCD specifies, in either of two forms, the alphanumeric characters to be drawn. The argument may (1) list the BCD characters; e.g., ..., 17HALFALPHANUMERIC DATA, ..., or (2) be the address of the first element of an array containing BCD characters; e.g., ..., BCDARY(1),
- THETA is the angle, in degrees, expressed in floating point at which the characters are to be written. THETA is measured counter-clockwise from the positive X axis; hence for THETA = 0.0, the characters are drawn left to right parallel to the X axis. For THETA = 0.0, the sine and cosine are not computed, but for any other angle, SIN and COS are called. If a string of characters is to be drawn at an angle other than 0.0, the entire string is rotated with the (X,Y) given in the calling sequence as the pivot plant.
- N is an integer which specifies the number of characters to be drawn.

If $N > 1$, spacing between the characters is accomplished automatically and is one-half the width of the characters.

The second function of this entry is to provide plotting of data points with the option of connecting consecutive data points with a straight line. The calling sequence is

CALL SYMBOL (X, Y, H, ICHAR, THETA, L),

where

- X is the abscissa, in inches, of the center of the character.
- Y is the ordinate, in inches, of the center of the character.
- H is the height, in inches, of the character and $H \geq 0.02$. Best results in this sequence will be obtained if H is an integral multiple of 0.02.
- ICCHAR is an integer which determines which symbol is to be plotted.
- THETA is the angle of rotation as previously described.
- L is a negative integer which indicates whether or not the points are to be connected with a straight line. If $L = -1$, the character will be plotted without a straight line being drawn from the previous (X, Y) position.

If $L < -1$, a straight line will be drawn from the previous (X, Y) to the given (X, Y) and the symbol will then be drawn. Note that L must be negative or the subroutine assumes a normal calling sequence as previously described. Only one character per entry is drawn in this calling sequence. At the completion of any of the centered symbols, the pen is at the (X, Y) position given in the calling sequence and the pen is DOWN.

Subroutine NUMBER. - This is a subroutine to convert a machine format number to its decimal equivalent and plot it according to a specified format. The calling sequence is

CALL NUMBER (S, Y, H, A, THETA, nHFORMAT),

where X, Y, H, and THETA are as described in the normal entry to subroutine SYMBOL. A is the name of the machine format number to be converted and

plotted. The type (integer or real) must conform to the FORMAT specified. NHFORMAT is a BCD argument which specifies the manner in which the number is to be converted and plotted. The NH portion of this argument is the normal FORTRAN method for transmitting BCD characters to a subroutine. The FORMAT portion is one of the four numeric format specifications I, E, F, or D. Examples of this argument are SHELO.5, 4HPC.3, 2HIS, 5HELO.3. The FORMAT specification must not exceed six characters, and scale factors must not be used. The total field width must not exceed 99 characters. The numbers are converted by the standard library conversion routines and are right-adjusted in the field. This subroutine is designed primarily for annotation where a single number is involved.

A2. Subroutine CRT for the Cathode Ray Tube Plotter

Subroutine CRT writes the plot commands on a 9-track tape for the cathode ray tube plotter. The basic calling sequence is

```
CALL CRT (ARG1, ARG2, IARG3, MODE)
```

The action taken depends on the value of MODE. The possible actions are described in the following sections and summarized in Table A1.

It is convenient to think of this plotter as writing on a page with a normal plotting area of 11" x 17" plus a margin on each side of about 1". If the user does not specify his own origin and scaling factors, the subroutine CRT will set up an 11" x 17" coordinate system with origin at the lower left corner of the normal plotting area. A request to move the beam from position (0.,0.) to position (4.,0.) will then produce a horizontal line along the bottom of the normal plotting area. Whether or not this line will be visible depends on the beam intensity requested for this beam movement.

Table A1. Summary of modes in CRT(ARG1, ARG2, IARG3, MODE)

ARG1 ¹	ARG2 ¹	IARG3 ²	MODE ³	ACTION
buffer name	buffer length (integer)	'your name\$'	0	Initialization
position X, Y		beam intensity indicator IZ	1 -1	Move the beam Find present beam coordinates
position X, Y dummy XDUM, YDUM		see Table 3 IBLOCK	2 -2	Write block numbers or advance film or close tape file Find last block number
XORG	YORG	beam intensity of 'set IZORG	3 -3	Change offset values Find present offset values
XFACT	YFACT	dummy IDUM	4 -4	Change scale factors Find present scale factors
position X, Y		point intensity indicator IZ	5	Plot a point
position X, Y		beam intensity indicator IZ	6	Ignore limit switches and move beam
dummy XDUM, YDUM		IZSET	7 -7	Change IZSET Find present IZSET

- 1 ARG1 and ARG2 are floating-point numbers, REAL*4 or REAL*8 (except when MODE=0).
- 2 IARG3 is a 4-byte integer (except when MODE=0).
- 3 MODE is a 4-byte integer.

As this line is produced on the cathode ray tube it is also recorded by a 35 mm camera. The film is advanced to a new frame for each new plot. Later, the film is developed and sent to the user.

Subroutine CRT may be called by Fortran programs and is included in the standard Fortran library on disk.

MODE=0, Initialization

```
CALL CRT (BUFFER,NBUFF,'YOUR NAME$',0)
```

This is an initialization call and must precede all other calls to CRT. Normally it is done only once and normally the subroutine will ignore further initialization calls. However, it is possible to force the system to reinitialize by setting NBUFF < 0.

BUFFER is the symbolic name of an array that CRT may use as an output buffer.

|NBUFF| is the number of 4-byte words in the array that CRT may use. Normally, it is the DIMENSION of BUFFER. 3000 ≤ NBUFF ≤ 5000 is recommended.

'YOUR NAME\$' Your name (12 characters or less) followed by a \$, within apostrophes. This will be used to plot a special identification frame on the film strip.

MODE=1, Moving the Beam and Plotting Lines

```
CALL CRT (X,Y,IZ,1)
```

X,Y represents the position to which the beam will be moved from its present position. However, X and Y will be translated and scaled, as described below. X and Y must be floating-point numbers, either single or double precision, REAL*4 or REAL*8.

IZ indicates the intensity to be used, as described below.

All movements are made to positions defined by coordinates relative to an origin. The initial origin (0.,0.) is always in the lower left corner of the normal plotting area. However, by using a call with MODE=3, a translated origin (XORG,YORG) may be obtained, and subsequent plotting

will be relative to the new origin. Each movement is made in a straight line approximation from the present position to a new position (ABSC,ORD) calculated from the first two arguments (X,Y) of the call statement. The coordinates are translated and scaled as follows:

$$ABSC = (X+XORG) *YFACT$$

$$ORD = (Y+YORG) *YFACT$$

(ABSC,ORD) are the translated and scaled coordinates, in inches, relative to the lower left corner.

(X,Y) are the first two arguments given in the calling sequence and represent the new position in the user's coordinate system.

(XORG,YORG) is the present position of the origin relative to the lower left corner, in user's units. XORG and YORG are initially 0. but they may be changed by a call with MODE=3.

XFACT and YFACT are scaling factors for abscissa and ordinate values respectively. For a movement parallel to the X-axis, XFACT *(distance in user's units) = distance in inches. XFACT and YFACT are initially 1.0 but they may be changed by a call with MODE=4. If XFACT=YFACT=1.0, a line of length 1.0 will be 1.0 inches long on an 11" x 17" print. If X and Y values both range from 0. to 100. and if one wants a square picture, then appropriate scaling factors are XFACT=YFACT=0.11.

With the Model 935 plotter it is possible to have 30 different intensity levels. The beam intensity is calculated from the third argument (IZ) in the call statement. If the value of IZ is zero, the beam is turned off. If the value is 99, the routine uses a value IZSET stored in the subroutine. IZSET may be changed by a call to CRT with MODE=7.

If IZ is not 0 or 99, the true beam intensity IZTRUE is IZ offset by the value of IZORG.

```

      IZTRUE = 0      if IZ = 0
      IZTRUE = IZ+IZORG  if IZ ≠ 0 and IZ ≠ 99
      IZTRUE = IZSET+IZORG  if IZ = 99

```

IZTRUE is the beam intensity request transmitted to the plotter.

IZ is the value specified by the argument in the call statement.

IZORG is a positive or negative intensity level offset. IZORG is initially 0 but may be changed by a call with MODE=3.

IZSET is a value stored for use when IZ=99. Initially, IZSET=16.

If IZTRUE is zero or negative, the beam will be turned off. If it is between 1 and 30, it is the intensity level used, and the beam will be turned on. If IZTRUE is greater than 30, the intensity used is $[(IZTRUE+1) \bmod 32 - 1]$.

IZTRUE=16 is a typical intensity for plotting lines. Intensities less than 7 are scarcely visible. A shift of four intensity units corresponds roughly to a factor of two change in brightness.

A line plotted with MODE=1 may not cross from inside to outside the normal plotting area. See Figure A1 and MODE=6.

MODE= -1

```
CALL CRT (XWHERE, YWHERE, IZWHAT, -1)
```

This call is used to return the values of the present beam location and intensity.

```

XWHERE,
YWHERE  is the present beam position, in the user's
        coordinate system.

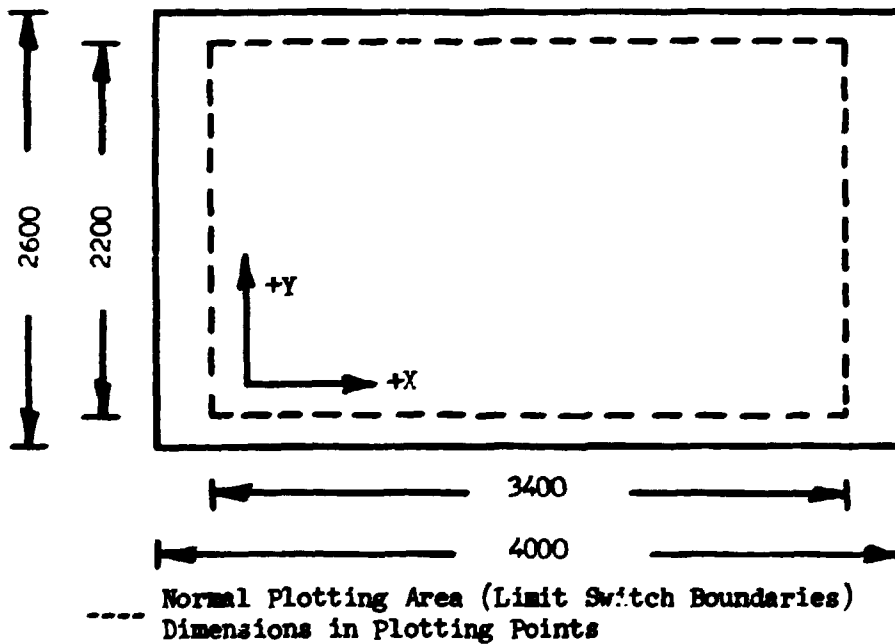
IZWHAT  is the present intensity level. This is
        the last positive non-zero value of IZTRUE
        used in plotting.

```

Table A2. Block numbers and film advance with CRT(X, Y, IB, 2)

Value of IB	Block Number Produced	Film Advance and Reorigin	Output Tape File Closed
0	Next Sequential Number	Yes	No
1-999	IB	Yes	No
1000	Next Sequential Number	No	No
1001-1999	IB - 1000	No	No
9000	Next Sequential Number	Yes	Yes
9001-9999	IB - 9000	Yes	Yes

Figure A1. Plotting area available



MODE=2, Ending a Graph

CALL CRT (X,Y,IB,2)

This call is used to generate block numbers. A block number is a separator between two adjacent graphs or plots on the tape. It is possible for the operator of the Model 835 plotter to search the plot tape for a particular block number and plot the corresponding graph.

A block number may be written with or without advancing the film. If the film is advanced, the origin for the next plot will be the final value of (XORG,YORG) of the present plot. A move to (X,Y) will always be made whether or not the film is advanced. The beam will always be turned off when the move is made.

X,Y is the position to which the beam will be moved.

IB is a four digit decimal number with a value from 0 to 9999. The three least significant digits specify the block number to be written. If nonzero, a block number consisting of those three digits will be written; if zero, the next sequential block number (starting with 1) will be written. The most significant digit is used to control film advance and to close the output file. If the most significant digit is zero, the film will be advanced. If it is 9, the output tape file will be closed and no further plotting commands may be written during the execution of this source program. See also Table A2; ranges of IB not described in Table A2 should not be used.

MODE= -2

CALL CRT (XDUM,YLUM,IBLOCK,-2)

This routine is used to return the value of the last block number that was used.

XDUM, YDUM are not used at this time.
IBLOCK is the last block number.

MODE=3, Changing the Origin

CALL CRT (XORG, YORG, IZORG, 3)

This call sets the internal values of XORG, YORG, and IZORG. It is used to establish a translated origin for subsequent movements. IZORG functions as a beam intensity origin. These values are all initialized at 0. If any of these values are changed, all subsequent movements will be made with the specified translation until the values are again changed by another call with MODE=3.

XORG, YORG is the new position of the origin relative to the lower left corner of the normal plotting area.
IZORG is the value to be used for translation of beam intensity.

MODE= -3

CALL CRT (XORG, YORG, IZORG, -3)

This call is used to return the current origin and beam translation values in effect.

XORG, YORG are the positions of the present origin relative to the lower left corner.
IZORG is the present translation value for beam intensity.

MODE=4, Changing Scale Factors

CALL CRT (XFACT, YFACT, IDUM, 4)

The purpose of this call is to set scaling factors for the X and Y coordinates. Scaling of abscissa and ordinate values are completely independent. XFACT and YFACT are both initialized with a value of 1.0.

If XFACT=YFACT=1.0, a line of length 1.0 will be 1.0 inches long on an 11" x 17" print.

XFACT is the scaling factor for the abscissa.
 YFACT is the scaling factor for the ordinate.
 IDUM is not used at this time.

MODE=4

CALL CRT (XFACT, YFACT, IDUM, 4)

This call returns the values of the scaling factors currently in use.

MODE=5, Plotting a Point

CALL CRT (XPOINT, YPOINT, IZ, 5)

This call moves the beam to the position (XPOINT, YPOINT) with the beam off and, when the beam arrives at that position, turns the beam on. This produces a point at the intensity level indicated by IZ at the position (XPOINT, YPOINT).

XPOINT, YPOINT is the position where the point will be produced.
 IZ indicates the intensity to be used, as for MODE=1.

As with MODE=1, the beam movement performed with MODE=5, may not cross from inside to outside the normal plotting area.

MODE=6, Plotting Outside the 11" x 17" Area

CALL CRT (X, Y, IZ, 6)

This call is used to bypass the limit switches and to plot outside the normal 11" x 17" area. Because of distortion outside the normal plotting area, this call should be used only for labelling or plotting

which does not require the full accuracy of the system. The action is done as for MODE=1, except that if MODE=6 the beam is allowed to pass the limit switch boundaries.

MODE=7, Changing IZSET

CALL CRT (XDUM, YDUM, IZSET, 7)

This call sets the internal parameter IZSET to any desired value.

XDUM, YDUM are not used.

IZSET This is the value of the intensity level to be used in calls with MODE=1, 5, or 6, and IZ=99, or in calls to CRTSYM. After translation, IZTRUE=IZSET+IZORG. IZSET is initialized at 16. If it is changed by this call, the new setting will remain in effect until changed again.

MODE= -7

CALL CRT (XDUM, YDUM, IZSET, -7)

This call returns the value stored in IZSET.

APPENDIX E

DESCRIPTION OF THE INPUT DATA

SIMTRAK I

Format for the Input Data Cards

Card No. (Format)	Field	Variable	Units	General Description
1 (20 M)	1-80	NTITLE	-	Headline for printed output and plots (only 1-60 used for plot title).
	1-10	R(1)	cm	outer radius of tube.
	11-20	WALL	cm	wall thickness (prior to oxidation).
	21-30	OLAYER(1)	cm	thickness of oxide layer at the outer surface. (Initial)
2 (6D10.9) (Initial geometry)	31-40	ALAYER(1)	cm	thickness of the alpha layer at the outer surface. (Initial)
	41-50	OLAYER(2)	cm	thickness of the oxide layer at the inner surface. (Initial)
	51-60	ALAYER(2)	cm	thickness at the alpha layer at the inner surface. (Initial)
3 (4D10.9,4I10) (Run conditions and output)	1-10	TMAX	sec	maximum time of experiment.
	11-20	DTEMP	sec	max. time step for temperature calculation (if 0, then DTEMP=DTPRIN will be set).
	21-30	DTDIFF	sec	max. time step for diffusion calculation (if 0, then DTDIFF=DTPRIN will be set).
	31-40	DTPRIN	sec	time step for printed output (can be function of time, then next variable > 0).
	41-50	NSTEP	-	number of changes in output time steps. (If > 0, then card 3A has to be supplied.)
	51-60	MPRINT	-	number of printed output steps between oxygen concentration - distance plots (not used if there are no plots of this type to be made).

Card No. (Format)	Field	Variable	Units	General Description
	61-70	NUMBER	-	identification number for first oxygen concentration-distance plot (if 0 then no plots of this type are made).
	71-80	NSCALE	-	NSCALE = 0 : Type A plots (y-axis: 0 to $\frac{200}{\text{cm}}$) NSCALE = 1 : Type B plots (y-axis: 0 to $0.5 \frac{200}{\text{cm}}$) NSCALE = 2 : Type A + Type B plots
3A (8D10.9) (card only if NSTEP > 0)	K-1, NSTEP	TDSTP(K)	sec	time at which change in output time step takes place.
		DTNEW(K)	sec	new output time step.
	1-10	NLUMB	-	NLUMB = 0 : complete temperature distribution in wall is calculated. NLUMB = 1 : uniform wall temperature, but calculated as function of heat transfer and heat generation. NLUMB = 2 : uniform wall temperature, set equal to TSTEAM(1) or TSTEAM(2) if TSTEAM(1) = 0.
4 (2H10) (Type of calculation)	11-20	NBAKER	-	NBAKER = 0 : oxygen distribution in wall is calculated. NBAKER = 1 : total oxygen calculation on basis of Baker-Just Eq. NBAKER = 2 : total oxygen calculation on basis of Hobson data. NBAKER = 3 : total oxygen calculation on basis of Lemmon Eq.

Card No. (Format)	Field	Variable	Units	General Description
5 (6D10.9) (Initial conditions at outer surface.)	1-10	HDIFF(1)	$\frac{\text{gram}}{\text{cm}^2 \cdot \text{sec}}$	upper limit for oxygen flux into the wall at the outer surface (if 0, then no oxidation at this surface).
	11-20	HCOOL(1)	$\frac{\text{W}}{\text{cm}^2 \cdot ^\circ\text{C}}$	convective heat transfer coefficient at the outer surface.
	21-30	TSTEAM(1)	$^\circ\text{C}$	coolant temperature at the outer surface.
	31-40	ERADIA(1)	-	thermal emissivity at the outer surface.
	41-50	TWALL(1)	$^\circ\text{C}$	temperature of surface to which outer surface is radiating.
	51-60	QFIXED(1)	$\frac{\text{W}}{\text{cm}^2}$	additional heat flux at outer surface (independent from HCOOL, TSTEAM, ERADIA, TWALL).
6 (6D10.9) (Initial conditions at inner surface.)				identical meaning as card 5 but for inner surface. (Either card 5 or card 6 can be empty if there is heat transfer and oxidation on one surface only.)
	1-10	NDIFIN(1)	-	number of oxygen flux limit-time pairs for outer surface (0 if constant).
7 (6D10) (Time dependent functions, outer surface.)	11-20	NCOEFF(1)		number of heat transfer coeff.-time pairs for outer surface (0 if constant).
	21-30	NTCOOL(1)		number of coolant temperature-time pairs for outer surface (0 if constant).
	31-40	NRADCO(1)		number of emissivity-time pairs for outer surface (0 if constant).
	41-50	NTWALL(1)		number of radiation temperature-time pairs for outer surface (0 if constant).
	51-60	NQFLUX(1)		number of heat flux-time pairs for outer surface (0 if constant).

Card No. (Format)	Field	Variable	Units	General Description
8 (0110) (Time dependent functions, inner surface)				identical meaning as card 7 but for inner surface. Either card 7 or 8 or both cards can be empty if there are no time functions. For each of the variables in card 7 or card 8 that is greater than 0, a corresponding card 0A to 0F or 10A to 10F has to be supplied.
0A (SD10.0)	K=1,NDIFIN(1)	NDIFIN(1,K)	TNDIF(1,K)	time functions for variables pertaining to outer surface.
0B (SD10.0)	K=1,NCOEFF(1)	HCOEFF(1,K)	TCOEFF(1,K)	omit if corresponding variable in card 7 is 0.
			 separate card(s) for each function.
0F (SD10.0)	K=1,NQFLUX(1)	QFLUX(1,K)	TQFLUX(1,K)	up to 25 cards for each type of pair can be used.
10A				identical meaning as cards 0A to 0F, but for inner surface.
			
10F			
	1-10	TSTART	°C	initial temperature in wall.
	11-20	CSTART	gram/cm ³	initial oxygen concentration in beta-phase.
	21-30	QSPLIT	$\frac{\text{wsec}}{\text{gram oxygen}}$	endothermic reaction heat for converting steam into oxygen and hydrogen, subtracted at the surface. (Full value is 15,650 wsec/gram O ₂)
11 (SD10.0, 40Y 110)	31-70	EMPTY		
	71-80	MPL0T		number of graphs and/or tables, to be plotted using variables determined as functions of time. (If 0, omit cards 12 and 13.)

Card No. (Format)	Field	Variable	Units	General Description
11 (11.0) (11.0) (11.0) (11.0) (11.0) (omit if MOUNT = Repeat card 11 for each graph H.L.MOUNT)	1-1	RELATE(X)	-	defined variable for X axis (see Table 10)
	11-1	SCALE(X)	units/in.	scale factor for X axis
	11-2	ORIG(X)	units of variable for X axis	value of X at origin (empty, if 0)
	11-3	NVAR(X)	-	number of X-axis variables plotted as a function of single X-axis variable. NVAR(X) = 1
	11-4	PLLOT(X)	-	determines if variables are plotted and/or printed: PLLOT = 0 : No plots; no print PLLOT = 1 : No plots; print PLLOT = 2 : Plots; no print PLLOT = 11 : Plots; print
	11-5	SCALE(Y)	in.	distance between Y axis and paper border. (generally, 1.0)
	11-6	DESCRIBE(X)	-	used to describe variable on X-axis
	11-7	RELATE(Y)	-	defined variable for Y axis (see Table 10)
	11-8	SCALE(Y)	units/in.	scale factor for Y axis (1" in. max. for Y-axis)
	11-9	ORIG(Y)	units of variable for Y axis	value of Y at origin (empty, if 0)
11 (11.0) (11.0) (11.0) (11.0) Repeat for each curve on graph H.L.MOUNT)	11-10	PLLOT(Y)	-	PLLOT = 0 : Points only are plotted PLLOT = 1 : Points are connected with a line
	11-11	DESCRIBE(Y) M.L.	-	used to describe variable on Y axis.

Table E1. Variables available for GRAPHICAL OUTPUT
 (Defined variables 3-12 refer to outer surface of tube;
 variables 13-22 refer to inner surface of tube.)

NPLOTX NPLOTY	VARIABLE	UNITS
1	time	sec.
2	square-root of time	(sec) ^{1/2}
3	steam (or coolant) temperature	°C
4	temp. of surface to which specimen is radiating	°C
5	surface temperature of specimen	°C
6	thickness of oxide layer	μm
7	thickness of alpha layer	μm
8	ξ-layer thickness (oxide + alpha)	μm
9	oxide/ξ ratio	-
10	oxygen gain	mg/cm ^{2*}
11	square of oxygen gain	(mg/cm ²) ^{2*}
12	square of ξ-layer thickness	(μm) ²
13-22	identical to 3-12 above, except that variable applies to inner surface of tube.	
23	total oxygen consumption	mg/cm ^{2*}
24	avg. oxygen concentration in Beta phase	g/cm ³
25	F _w , beta layer thickness/orig. wall thickness	-

*area reference is outer surface.

APPENDIX C

DESCRIPTION OF THE OUTPUT DATA

In addition to the printing of the input data, (except for cards 3a, 9a-9f, 10a-10f, 12, and 13), and tables of values of the materials properties utilized for each run, the following variables are printed for each specified time step (where applicable, for both inner and outer tube surfaces):

TIME	[sec]	Oxidation time.
PLOT NO.	[-]	Identification number for oxygen concentration profile plots (0 if there are no plots of this type).
H.T. COEFF	$[\frac{W}{cm^2 \cdot K}]$	Convective heat transfer coefficient.
STEAM TEMP	[°C]	Steam temperature.
EMISSIVITY	[-]	Thermal emissivity.
RAD. WALL	[°C]	Temperature of surroundings with which radiation heat is exchanged.
SURFACE TEMP	[°C]	Surface temperature of Zircaloy.
OX/MET TEMP	[°C]	Temperature at the oxide/ α interface.
FIX. HEATFLUX	$[\frac{W}{cm^2}]$	Fixed heat flux at the surface of the Zircaloy (in addition to convection and radiation).
CON. HEATFLUX	$[\frac{W}{cm^2}]$	Convective heat flux.
RAD. HEATFLUX	$[\frac{W}{cm^2}]$	Radiative heat flux.
QCON + QRAD	$[\frac{W}{cm^2}]$	Sum of radiative and convective heat fluxes.
O. FL. LIMIT	$[\frac{gram}{cm^2 \cdot sec}]$	Upper limit for oxygen flux; identical with HDIFF.
OXYGEN FLUX	$[\frac{mg}{cm^2 \cdot sec}]$	Actual (instantaneous) oxygen flux.
O. IN OXID	$[\frac{mg}{cm^2}]$	Oxygen content in oxide layer.
O. IN ALPHA	$[\frac{mg}{cm^2}]$	Oxygen content in α layer.

O. IN BETA	$[\frac{\mu\text{g}}{\text{cm}^2}]$	Oxygen content in remaining β layer.
OXYG. TOTAL*	$[\frac{\mu\text{g}}{\text{cm}^2}]$	Total oxygen content.
OXYG. GAIN*	$[\frac{\mu\text{g}}{\text{cm}^2}]$	Oxygen gain.
OXIDE LAYER	$[\mu\text{m}]$	Thickness of oxide layer.
ALPHA LAYER	$[\mu\text{m}]$	Thickness of α layer.
BETA LAYER	$[\mu\text{m}]$	Thickness of β layer.

If there is oxidation and/or heat transfer on both surfaces, the first line of the variables is for the outer surface, the second line for the inner surface. In each case, the variables O.IN OXIDE to OXYG.GAIN are calculated with the outer surface as reference area.

In addition, for each calculated node the following variables are printed out:

POINT NUMBER	$[-]$	Number of the node which indicates the position from the outer surface.
DISTANCE	$[\text{cm}]$	Distance of the node from the original outer surface. Since the volume of the oxide is larger than the volume of unoxidized Zircaloy, DISTANCE will be negative for some point(s) if oxidation occurs at the outer surface.
TEMPERATURE	$[^{\circ}\text{C}]$	Temperature of the node.
CONCENTRATION	$[\frac{\mu\text{gram}}{\text{cm}^3}]$	Oxygen concentration in the node.

*Note: OXYG.TOTAL is determined by an integration of the oxygen concentration over the entire wall for each output time. OXYG.GAIN is determined by an integration of instantaneous flux over the time. The difference between the two variables can vary slightly from the value of the initial oxygen content (OXYG.TOTAL = 0) due to numerical inaccuracy.

APPENDIX D

EXAMPLE PROBLEMS

Three test cases have been selected as sample problems to illustrate the preparation of the input and to show typical output results.

Test Case 1. A Comparison of a SIMTRAN Result with an Analytical Solution

A simple nonmoving-boundary diffusion problem was chosen since there are no analytical solutions known for the problem of the two moving boundaries in a wall with a finite thickness. To enable a comparison to be made, the code was "degraded" by giving all three layers the same material properties. The properties of beta-Zircaloy were used for the basis material. The concentration at the "interfaces" was set arbitrarily at 75% and 25% of the equilibrium oxygen concentration. The initial and the boundary conditions for the problem were chosen as:

$$T = \text{constant} = 1400^{\circ}\text{C}$$

$$\text{at } \tau = 0:$$

$$C = 0.00649 \text{ for } 0 < x \leq l$$

$$C = C_{\beta/\alpha} = 0.058556 \text{ for } x = 0$$

$$\text{at } x = 0:$$

$$C = C_{\beta/\alpha} \quad \text{for } 0 \leq \tau \leq \tau_{\text{MAX}}$$

$$\text{at } x = l:$$

$$\frac{\partial C}{\partial x} = 0 \quad \text{for } 0 \leq \tau \leq \tau_{\text{MAX}}$$

The analytical solution $C(x, \tau)$ is given by:

$$C = C_0 + \{C_s - C_0\} \left\{ 1 - \frac{4}{\pi} \sum_{n=0}^{\infty} \frac{1}{2n+1} \sin \left[\frac{(2n+1)\pi x}{l} \right] \exp \left[-\frac{(2n+1)^2 \pi^2 D \tau}{l^2} \right] \right\} \quad (D1)$$

The results of Eq. (D1) are plotted in Fig. D1 for $\tau = 5, 15,$ and 60 sec. Also shown in this figure are a number of concentration values calculated with SIMTRAN. The agreement is seen to be quite good.

Table D1 shows the complete listing of the input data and the output for three selected times. The computing time for this problem was 27 sec on an IBM 360/91.

Test Case 2. Isothermal Reaction at 1000°C (1832°F), Two-Side Oxidation

This case simulates an ideal isothermal oxidation experiment at 1000°C (1832°F) with an oxidation time of 30 min. Figure D2 shows the thickness of the oxide and ξ (oxide plus alpha) layers as functions of time. Figures D3 and D4 show the concentration profiles across the wall after 30 minutes in two different scales. The input data and the output data for three selected times are listed in Table D2. The computing time was 13 sec.

Test Case 3. Burst Test of a Zircaloy Tube in Steam

This case represents an application of SIMTRAN to a simple tube-burst problem. In this problem, a Zircaloy tube is visualized as being heated by an internal electrical heater having a constant rate of temperature increase. The gap between tube and heater assumed to be filled with helium under pressure. The intention is to cut off the electrical power as soon as the tube bursts in order to measure the existing deformation. The test is assumed to be made in a steam environment. The question was: can the steam-Zircaloy reaction generate sufficient heat at higher temperatures so that the Zircaloy temperature would continue to rise even after the heater power was cut off?

The calculation has been made with no initial oxide layer which leads to the maximum reaction. Heat transfer to the steam has been neglected for simplicity, (although it could be considered if desired).

The Zircaloy temperature and the temperature of the heater surface are plotted vs time in Fig. D5. In the same figure the penetration of the α/β -interface into the wall is shown. Figure D6 shows the oxygen concentration in the α and β phases after 35 sec. Input and output are listed in Table D3. Computing time was 11 sec.

In order to show the difference between the lumped temperature calculation (NLUMB=1), where the entire wall is treated as a single node and the more detailed calculation (NLUMB=0), where the complete temperature profile in the wall is calculated, test case 3 was repeated as case 3A with NLUMB=0.* The output for three selected time steps for this latter case is printed in Table D4.

*The computing time increased by a factor of 3.

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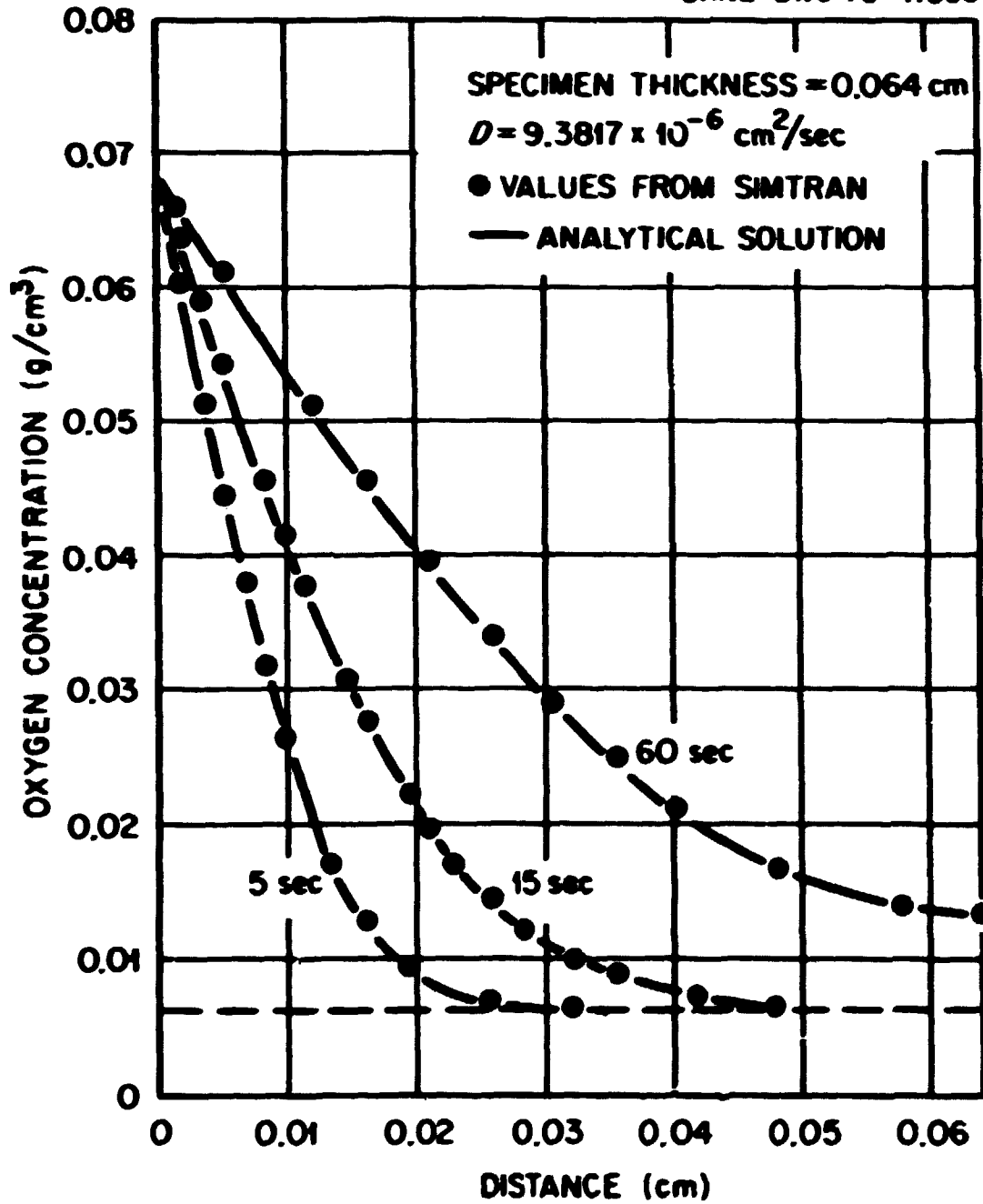


Fig. D1. Comparison of SIMTRAN result with analytical solution for single-phase, nonmoving-boundary case. Test Case 1.

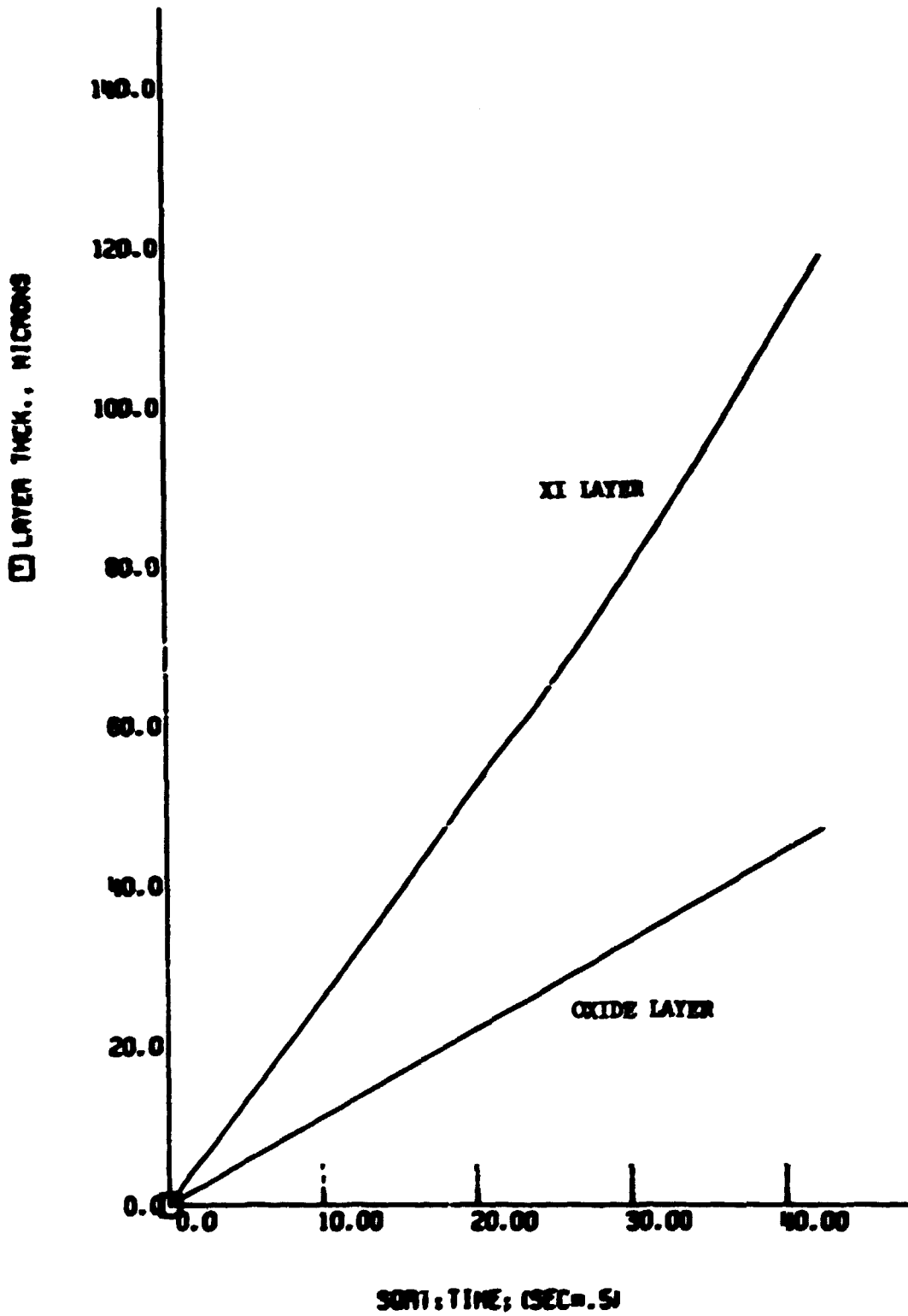
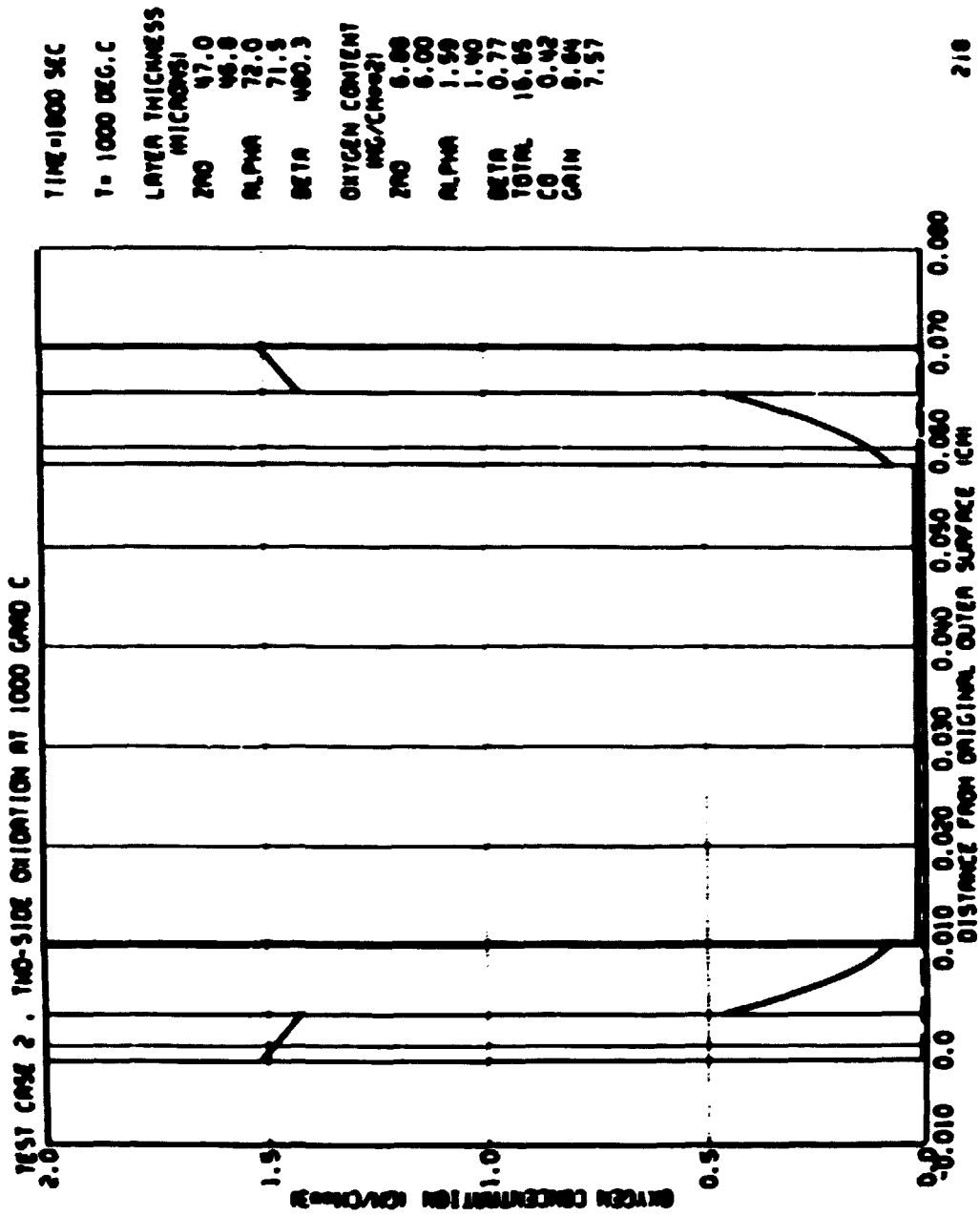


Fig. D2. Ideal isothermal oxidation curves. Test Case 2.



TIME=1000 SEC
 T= 1000 DEG.C
 LAYER THICKNESS
 MICRONS:
 ZRO 47.0
 ALPHA 46.0
 ALPMA 72.0
 BETA 71.5
 BETA 400.3
 OXYGEN CONTENT
 MG/CM²:
 ZRO 6.00
 ALPHA 6.00
 ALPMA 1.50
 BETA 1.40
 BETA 0.77
 TOTAL 16.05
 CO 0.42
 GAIN 0.84
 7.57

Fig. D3. Oxygen concentration in oxide, α - and β -Zirconalloy. Test Case 2.

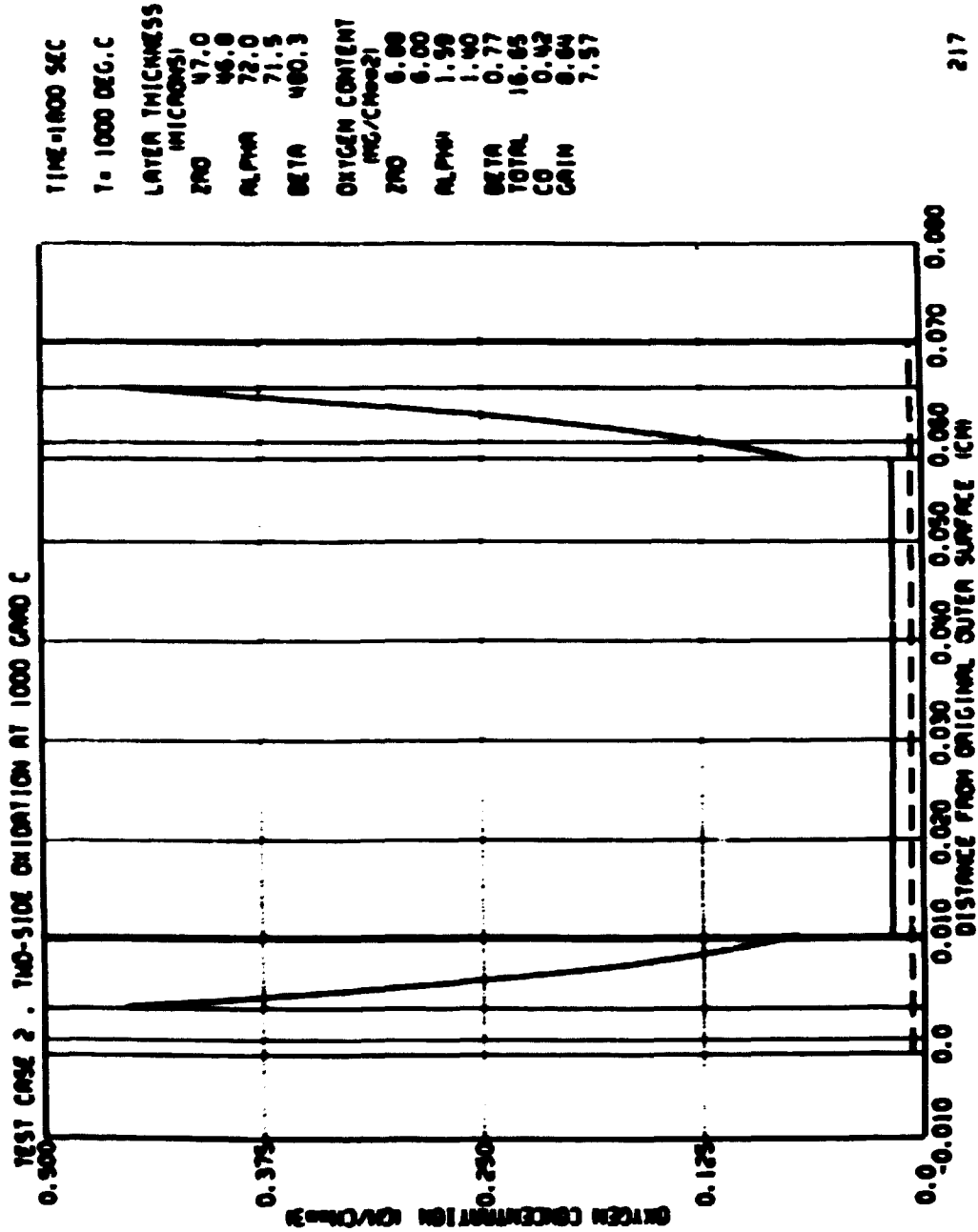


Fig. D4. Oxygen concentration in α - and β -Zircaloy. Test Case 2.

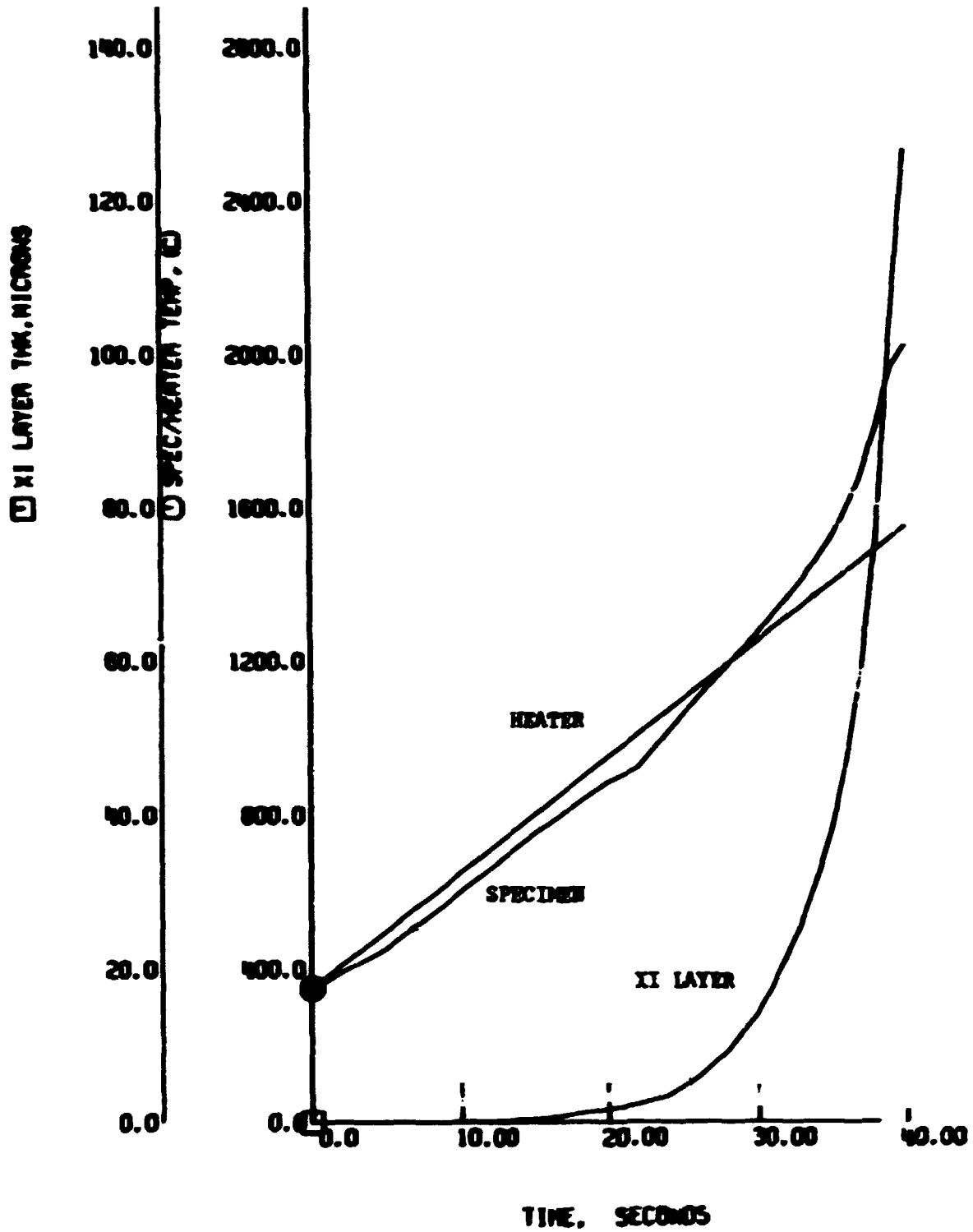
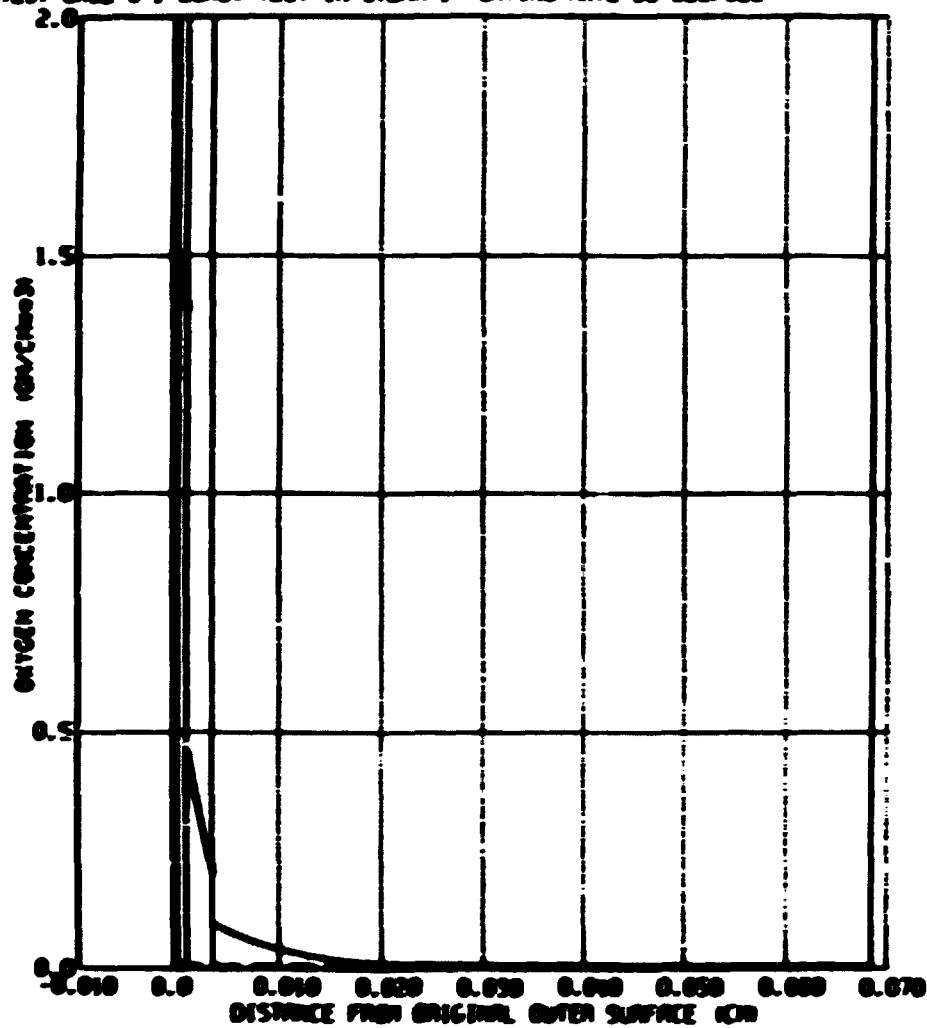


Fig. D5. Temperature and layer thickness variations. Test Case 3.

TEST CASE 3 . BURST TEST IN STEAM . HEATING RATE 30 DEG/SEC



TIME = 35 SEC

T = 1522 DEG.C

LAYER THICKNESS
(MICRONS)

ZNO 12.7

ALPHA 25.7

BETA 651.9

OXYGEN CONTENT
(WT-%)

ZNO 1.03

ALPHA 0.01

BETA 0.92

TOTAL 3.57

CO 0.42

GRN 3.14

314

Fig. D6. Oxygen concentration in oxide, α - and β -Zircaloy. Test Case 3.

• • • TIME = 9,300 • • •

PLOT # = 0

H.T. COEFF	STEAM FLOW	PERMISSIVITY	RAD. WALL	SURFACE TEMP	HEAT TEMP	FIN. HEATFLUX	CON. HEATFLUX	RAD. HEATFLUX	CONV. GRAD
0.0	1000.00000	0.0	0.0	1000.00000	1000.00000	0.0	0.0	0.0	0.0
0.0	0.0	0.0	0.0	1000.00000	1000.00000	0.0	0.0	0.0	0.0
O. PL. LIMIT	OUTSIDE FLUX	O. IN OXIDE	O. IN ALPHA	O. IN BETA	OVG. TOTAL	OVG. GAIN	OXIDE LAYER	ALPHA LAYER	BETA LAYER
10.0000	0.0076	0.7524	0.1100	0.1021	0.0047	0.0700	11.0077	00.0702	000.0211

OUTSIDE OXIDE LAYER

POINT NUMBER	1	17	34
DISTANCE	0.0	0.00100	0.00170
TEMPERATURE	1000.00	1000.00	1000.00
CONCENTRATION	0.00000	0.00023	0.00127

OUTSIDE ALPHA LAYER

POINT NUMBER	35	40	45	51	57	113	131
DISTANCE	0.00170	0.00200	0.00200	0.00200	0.00200	0.01120	0.01200
TEMPERATURE	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00
CONCENTRATION	0.00127	0.00093	0.00093	0.00101	0.00215	0.00102	0.00100

BETA LAYER

POINT NUMBER	131	161	191	225	247	290	321	343	364	417	449	481	513
DISTANCE	0.01200	0.01400	0.01020	0.02200	0.02400	0.02400	0.03200	0.03520	0.03000	0.00100	0.00000	0.00000	0.00120
TEMPERATURE	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00
CONCENTRATION	0.00100	0.00100	0.00100	0.00100	0.00100	0.00100	0.00100	0.00100	0.00100	0.00100	0.00100	0.00100	0.00100

BETA LAYER

POINT NUMBER	505	577	609	641
DISTANCE	0.04000	0.04700	0.00000	0.00000
TEMPERATURE	1000.00	1000.00	1000.00	1000.00
CONCENTRATION	0.00000	0.00000	0.00000	0.00000

• • • TIME = 14,300 • • •

PLOT # = 0

H.T. COEFF	STEAM FLOW	PERMISSIVITY	RAD. WALL	SURFACE TEMP	HEAT TEMP	FIN. HEATFLUX	CON. HEATFLUX	RAD. HEATFLUX	CONV. GRAD
0.0	1000.00000	0.0	0.0	1000.00000	1000.00000	0.0	0.0	0.0	0.0
0.0	0.0	0.0	0.0	1000.00000	1000.00000	0.0	0.0	0.0	0.0
O. PL. LIMIT	OUTSIDE FLUX	O. IN OXIDE	O. IN ALPHA	O. IN BETA	OVG. TOTAL	OVG. GAIN	OXIDE LAYER	ALPHA LAYER	BETA LAYER
10.0000	0.0277	0.3524	0.0020	0.1120	1.7077	0.0700	10.0076	100.1700	011.1900

OUTSIDE OXIDE LAYER

POINT NUMBER	1	17	33	49	60
DISTANCE	0.0	0.00100	0.00170	0.00200	0.00170
TEMPERATURE	1000.00	1000.00	1000.00	1000.00	1000.00
CONCENTRATION	0.00000	0.00100	0.00000	0.00000	0.00127

OUTSIDE ALPHA LAYER

POINT NUMBER =	60	81	97	113	129	145	161	177	193	209	230
DISTANCE =	0.00590	0.00800	0.00960	0.01120	0.01280	0.01440	0.01600	0.01760	0.01920	0.02080	0.02200
TEMPERATURE =	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00
CONCENTRATION =	0.05127	0.04575	0.04163	0.03773	0.03408	0.03068	0.02756	0.02471	0.02215	0.01987	0.01709

BETA LAYER

POINT NUMBER =	230	257	289	321	353	385	417	449	481	513	545	577	609
DISTANCE =	0.02288	0.02560	0.02880	0.03200	0.03520	0.03840	0.04160	0.04480	0.04800	0.05128	0.05448	0.05760	0.06080
TEMPERATURE =	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00
CONCENTRATION =	0.01709	0.01461	0.01207	0.01010	0.00885	0.00795	0.00717	0.00760	0.00670	0.00645	0.00657	0.00654	0.00652

BETA LAYER

POINT NUMBER =	641
DISTANCE =	0.06400
TEMPERATURE =	1400.00
CONCENTRATION =	0.00651

* * * * TIME = 60.000 * * * *

PLOT # = 0

W.T. COEFF	STEAM PERP	WISSIVITY	RAD. WALL	SURFACE TEMP	OX/NET TEMP	FIX. WEA	LUX	CON. HEATFLUX	RAD. HEATFLUX	OCOM*QPAD
0.0	1400.00000	0.0	0.0	1400.00000	1400.00000	0.	0.0	0.0	0.0	0.0
0.0	0.0	0.0	0.0	1400.00000	1400.00000	0.0	0.0	0.0	0.0	0.0
O. PL. LIMIT	OXYGEN FLUX	O. IN OXIDE	O. IN ALPHA	O. IN BETA	OXYG. TOTAL	OXYG. GAIN	OXIDE LAYER	ALPHA LAYER	BETA LAYER	
10.0000	0.0137	0.7099	1.1277	0.2304	2.0742	1.4508	110.8493	340.1670	160.9829	

OUTSIDE OXIDE LAYER

POINT NUMBER =	1	17	33	49	65	81	97	113
DISTANCE =	0.0	0.00160	0.00320	0.00480	0.00640	0.00800	0.00960	0.01120
TEMPERATURE =	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00
CONCENTRATION =	0.04838	0.06601	0.08367	0.06134	0.05903	0.05674	0.05448	0.05127

OUTSIDE ALPHA LAYER

POINT NUMBER =	120	129	145	161	177	193	209	225	241	257	273	289	305
POINT NUMBER =	321	337	353	369	385	401	417	433	449	465	481	497	513
DISTANCE =	0.01188	0.01280	0.01440	0.01600	0.01760	0.01920	0.02080	0.02240	0.02400	0.02560	0.02720	0.02880	0.03040
DISTANCE =	0.03200	0.03360	0.03520	0.03680	0.03840	0.04000	0.04160	0.04320	0.04480	0.04640	0.04798	0.04958	0.05118
TEMPERATURE =	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00
TEMPERATURE =	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00
CONCENTRATION =	0.05127	0.05002	0.04787	0.04576	0.04370	0.04169	0.03973	0.03784	0.03601	0.03424	0.03254	0.03091	0.02935
CONCENTRATION =	0.02786	0.02645	0.02511	0.02384	0.02265	0.02153	0.02049	0.01952	0.01863	0.01781	0.01709		

BETA LAYER

POINT NUMBER =	480	513	545	577	609	641
DISTANCE =	0.04790	0.05120	0.05440	0.05760	0.06080	0.06400
TEMPERATURE =	1400.00	1400.00	1400.00	1400.00	1400.00	1400.00
CONCENTRATION =	0.01709	0.01593	0.01493	0.01422	0.01379	0.01345

*** TIME = 200.000 ***

PLOT 1 = 201

H.T.CORFF	STRAN TEMP	EMISSIVITY	RAD.WALL	SURFACE TEMP	OX/NET TEMP	PIX.HEATFLUX	CON.HEATFLUX	RAD.HEATFLUX	QCON+QWAB
0.0	1000.00000	0.0	0.0	1000.00000	1000.00000	0.0	0.0	0.0	0.0
0.0	0.0	0.0	0.0	1000.00000	1000.00000	0.0	0.0	0.0	0.0

O.PL.LIMIT	OXIGEN FLUX	O.IN OXIDE	O.IN ALPHA	O.IN BETA	OXYG.TOTAL	OXYG.GAIN	OXIDE LAYER	ALPHA LAYER	BETA LAYER
1.0000	0.0072	2.2844	0.4942	0.6242	5.8249	2.8786	15.5813	21.0281	623.3042
1.0000	0.0073	1.9907	0.4314	0.0	0.0	2.5111	15.5553	20.9291	0.0

OUTSIDE OXIDE LAYER

POINT NUMBER	DISTANCE	TEMPERATURE	CONCENTRATION
1	-0.00052	1000.00	1.51400
5	0.00012	1000.00	1.47561
9	0.00077	1000.00	1.43711
11	0.00103	1000.00	1.42151

OUTSIDE ALPHA LAYER

POINT NUMBER	DISTANCE	TEMPERATURE	CONCENTRATION
11	0.00103	1000.00	0.45365
13	0.00129	1000.00	0.39096
17	0.00172	1000.00	0.29136
21	0.00218	1000.00	0.20850
25	0.00257	1000.00	0.14365
30	0.00314	1000.00	0.07010

BETA LAYER

POINT NUMBER	DISTANCE	TEMPERATURE	CONCENTRATION
30	0.00314	1000.00	0.01738
41	0.00429	1000.00	0.01669
57	0.00515	1000.00	0.01618
57	0.00600	1000.00	0.01567
65	0.00686	1000.00	0.01518
73	0.00772	1000.00	0.01469
81	0.00858	1000.00	0.01422
89	0.00943	1000.00	0.01376
97	0.01029	1000.00	0.01331
105	0.01115	1000.00	0.01288
113	0.01201	1000.00	0.01246
129	0.01372	1000.00	0.01167
193	0.02058	1000.00	0.00920

BETA LAYER

POINT NUMBER	DISTANCE	TEMPERATURE	CONCENTRATION
257	0.02744	1000.00	0.00785
321	0.03430	1000.00	0.00742
385	0.04116	1000.00	0.00700
449	0.04802	1000.00	0.00692
513	0.05488	1000.00	0.01156
529	0.05660	1000.00	0.01235
537	0.05745	1000.00	0.01277
545	0.05831	1000.00	0.01321
553	0.05917	1000.00	0.01366
561	0.06003	1000.00	0.01413
569	0.06088	1000.00	0.01461
577	0.06174	1000.00	0.01511
585	0.06260	1000.00	0.01562

BETA LAYER

POINT NUMBER	DISTANCE	TEMPERATURE	CONCENTRATION
593	0.06346	1000.00	0.01613
601	0.06431	1000.00	0.01666
612	0.06546	1000.00	0.01738

INSIDE ALPHA LAYER

POINT NUMBER	DISTANCE	TEMPERATURE	CONCENTRATION
612	0.06546	1000.00	0.07010
617	0.06603	1000.00	0.14226
621	0.06666	1000.00	0.20723
625	0.06689	1000.00	0.29029
629	0.06731	1000.00	0.39021
631	0.06757	1000.00	0.45365

INSIDE OXIDE LAYER

POINT NUMBER	DISTANCE	TEMPERATURE	CONCENTRATION
631	0.06757	1000.00	1.42151
633	0.06783	1000.00	1.43697
637	0.06848	1000.00	1.47531
641	0.06912	1000.00	1.51400

* * * TIME = 600.000 * * *

PLOT # = 205

N.T.COEFF	STEAM TEMP	EMISSIVITY	RAD.WALL	SURFACE TEMP	OI/NET TEMP	FIX.HEATFLUX	CON.HEATFLUX	RAD.HEATFLUX	OCOR+ORAD
0.0	1000.0000	0.0	0.0	1000.0000	1000.0000	0.0	0.0	0.0	0.0
0.0	0.0	0.0	0.0	1000.0000	1000.0000	0.0	0.0	0.0	0.0
O.FL.LIMIT	OXIGEN FLUX	O.IN OXIDE	O.IN ALPHA	O.IN BETA	OKYG.TOTAL	OKYG.GAIN	OXIDE LAYER	ALPHA LAYER	BETA LAYER
1.0000	0.0042	3.9575	0.8707	0.7591	9.7983	4.9925	27.0116	36.7061	576.0701
1.0000	0.0042	3.4496	0.7615	0.0	0.0	4.3632	26.9320	36.5432	0.0

OUTSIDE OXIDE LAYER

POINT NUMBER =	1	9	18
DISTANCE =	-0.00091	0.00038	0.00179
TEMPERATURE =	1000.00	1000.00	1000.00
CONCENTRATION =	1.51400	1.46941	1.42151

OUTSIDE ALPHA LAYER

POINT NUMBER =	19	25	33	41	52
DISTANCE =	0.00179	0.00257	0.00343	0.00429	0.00517
TEMPERATURE =	1000.00	1000.00	1000.00	1000.00	1000.00
CONCENTRATION =	0.45365	0.34759	0.24159	0.16212	0.07010

BETA LAYER

POINT NUMBER =	52	65	81	97	113	129	145	161	177	193	209	225	241
DISTANCE =	0.00547	0.00684	0.00858	0.01029	0.01201	0.01372	0.01544	0.01715	0.01887	0.02058	0.02230	0.02404	0.02576
TEMPERATURE =	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00
CONCENTRATION =	0.01738	0.01699	0.01650	0.01603	0.01557	0.01512	0.01470	0.01430	0.01393	0.01359	0.01328	0.01297	0.01268

BETA LAYER

POINT NUMBER =	385	433	489	545	601	657	713	769	825	881	937	993
DISTANCE =	0.04116	0.04631	0.04802	0.04974	0.05145	0.05317	0.05488	0.05660	0.05831	0.06003	0.06174	0.06346
TEMPERATURE =	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00
CONCENTRATION =	0.01251	0.01319	0.01349	0.01383	0.01420	0.01460	0.01503	0.01549	0.01596	0.01645	0.01694	0.01738

INSIDE ALPHA LAYER

POINT NUMBER =	590	601	609	617	624
DISTANCE =	0.06316	0.06431	0.06517	0.06603	0.06681
TEMPERATURE =	1000.00	1000.00	1000.00	1000.00	1000.00
CONCENTRATION =	0.07010	0.15967	0.23924	0.34578	0.45365

INSIDE OXIDE LAYER

POINT NUMBER =	624	633	641
DISTANCE =	0.06681	0.06821	0.06951
TEMPERATURE =	1000.00	1000.00	1000.00
CONCENTRATION =	1.42151	1.46944	1.51400

* * * TIME = 1000.000 * * *

PLOT 0 = 317

H.T.COEFF	STEAM TEMP	EMISSIVITY	RAD.WALL SURFACE TEMP	OX/NER TEMP	FIX.HEATFLUX	CON.HEATFLUX	RAD.HEATFLUX	OCOM*GRAD	
0.0	1000.00000	0.0	0.0	1000.00000	1000.00000	0.0	0.0	0.0	
0.0	0.0	0.0	0.0	1000.00000	1000.00000	0.0	0.0	0.0	
O.FL.LIMIT	OXIGEN FLOW	O.IN OXIDE	O.IN ALPHA	O.IN BETA	OXYG.TOTAL	OXYG.GAIN	OXIDE LAYER	ALPHA LAYER	BETA LAYER
1.0000	0.0024	6.8833	1.5888	0.7709	16.6511	8.6370	47.0397	71.9781	480.2545
1.0000	0.0024	6.0037	1.4045	0.0	0.0	7.5694	46.8105	71.4895	0.0

OUTSIDE OXIDE LAYER

POINT NUMBER =	1	9	17	25	30
DISTANCE =	-0.00158	-0.00029	0.00100	0.00229	0.00312
TEMPERATURE =	1000.00	1000.00	1000.00	1000.00	1000.00
CONCENTRATION =	1.51400	1.48845	1.46296	1.43762	1.42151

OUTSIDE ALPHA LAYER

POINT NUMBER =	30	41	49	57	65	73	81	89	97
DISTANCE =	0.00312	0.00429	0.00515	0.00600	0.00686	0.00772	0.00858	0.00943	0.01032
TEMPERATURE =	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00
CONCENTRATION =	0.45365	0.36161	0.29740	0.24145	0.19357	0.15330	0.12016	0.09384	0.07010

BETA LAYER

POINT NUMBER =	97	113	129	145	161	177	193	209	225	241	257	273	289
DISTANCE =	0.01032	0.01201	0.01372	0.01544	0.01715	0.01887	0.02058	0.02230	0.02401	0.02573	0.02744	0.02916	0.03088
TEMPERATURE =	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00
CONCENTRATION =	0.01738	0.01734	0.01730	0.01727	0.01723	0.01720	0.01717	0.01714	0.01712	0.01710	0.01708	0.01706	0.01707

BETA LAYER

POINT NUMBER =	401	417	433	449	465	481	497	513	529	545
DISTANCE =	0.04288	0.04459	0.04631	0.04802	0.04974	0.05145	0.05317	0.05488	0.05660	0.05834
TEMPERATURE =	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00
CONCENTRATION =	0.01709	0.01711	0.01713	0.01716	0.01719	0.01723	0.01726	0.01730	0.01734	0.01738

INSIDE ALPHA LAYER

POINT NUMBER =	545	553	561	569	577	585	593	601	612
DISTANCE =	0.05834	0.05917	0.06003	0.06088	0.06174	0.06260	0.06346	0.06431	0.06549
TEMPERATURE =	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00	1000.00
CONCENTRATION =	0.07010	0.09200	0.11818	0.15112	0.19118	0.23888	0.29477	0.35926	0.45365

INSIDE OXIDE LAYER

POINT NUMBER =	612	617	625	633	641
DISTANCE =	0.06549	0.06630	0.06739	0.06888	0.07010
TEMPERATURE =	1000.00	1000.00	1000.00	1000.00	1000.00
CONCENTRATION =	1.42151	1.43719	1.46258	1.48822	1.51400

TABLE D3. SELECTED INPUT-OUTPUT FOR TEST CASE 7: SIMULATED WIRETEST OF ZINCOLOY TUBE IN STEAM.

```

SOFT      WALL DOXID(1)  CALPA(1)  DOXID(2)  SALPA(2)
0.53200  0.06860  0.0      0.0      0.0
TRAX      DTTEMP  DTDIFF  DTRPM  NSTEP  MPRINT  NUMBER  MSCALE
0.0       0.0      0.0      3.0000  2       1       301      0
MURB      MURBEB
1         0
MZIPF(H)  MCOOL(H)  TSTAR(H)  IRADIA(H)  TWALL(H)  QFIBD(H)
1.0000   0.0      0.0      0.0      0.0      0.0
0.0      0.1000  350.0000  0.0      0.0      0.0
MZIPR(H)  MCOEPP(H)  MCOOL(H)  MRADCO(H)  MWALL(H)  MOPLEX(H)
0         0      2         0         0         0
0         0
RSTART    CSTART    QSPLIT
330.00   0.006630  0.0
    
```

MPILOT
1

*** MATERIAL PROPERTIES ***

```

METAL DENSITY = 6.890  OXID DENSITY = 5.820  GRAM/CM**3  REACTION HEAT = 34330.00  EBEC/GRAM OXIDEM
TEMP.(C)  STOCH.O2  OX.FAL.  AL./OXA  METAL/AL.  OXID  ALPHA  BETA  METAL  METAL  METAL
750.00    1.51800  1.46026  0.45365  0.00816  0.00391  0.0720-08  0.7218-10  0.4298-07  0.19377  0.61755  0.26530
800.00    1.51800  1.43451  0.45365  0.00816  0.00391  0.1020-07  0.2148-09  0.6188-07  0.20783  0.62000  0.26530
850.00    1.51800  1.42276  0.45365  0.00816  0.00391  0.2008-07  0.3775-09  0.1478-06  0.23137  0.62231  0.26530
900.00    1.51800  1.42901  0.45365  0.03010  0.00800  0.3019-07  0.1708-08  0.2329-06  0.22502  0.62760  1.20000
950.00    1.51800  1.42526  0.45365  0.05073  0.01289  0.7009-07  0.4330-08  0.4109-04  0.20877  0.62095  0.26530
1000.00   1.51800  1.42151  0.45365  0.07010  0.01738  0.1318-06  0.9495-08  0.6338-04  0.26252  0.62420  0.26530
1050.00   1.51800  1.41776  0.45365  0.08815  0.02157  0.2008-06  0.2118-07  0.9958-04  0.27657  0.61745  0.26530
1100.00   1.51800  1.41401  0.45365  0.10691  0.02637  0.3198-06  0.4278-07  0.1478-05  0.29002  0.64160  0.26530
1150.00   1.51800  1.41026  0.45365  0.12030  0.03170  0.4928-06  0.6218-07  0.2119-05  0.30377  0.64435  0.26530
1200.00   1.51800  1.40651  0.45365  0.13524  0.03702  0.7348-06  0.9518-06  0.2979-05  0.31712  0.64770  0.26530
1250.00   1.51800  1.40276  0.45365  0.14792  0.04249  0.1078-05  0.2678-06  0.4078-05  0.33137  0.65165  0.26530
1300.00   1.51800  1.39901  0.45365  0.15859  0.05101  0.1538-05  0.4558-06  0.5678-05  0.34502  0.65440  0.26530
1350.00   1.51800  1.39526  0.45365  0.16927  0.05977  0.2139-05  0.7518-06  0.7229-05  0.35877  0.65775  0.26530
1400.00   1.51800  1.39151  0.45365  0.17826  0.06836  0.3008-05  0.1208-05  0.9308-05  0.37252  0.66110  0.26530
1450.00   1.51800  1.38776  0.45365  0.18595  0.07357  0.3308-05  0.1878-05  0.1308-04  0.20637  0.64405  0.26530
1500.00   1.51800  1.38401  0.45365  0.19236  0.07741  0.4338-05  0.2858-05  0.1518-04  0.4002  0.65780  0.26530
1550.00   1.51800  1.38026  0.45365  0.19790  0.07905  0.6668-05  0.4235-05  0.1098-04  0.41377  0.67115  0.26530
    
```

*** TIME = 20.000 ***

PLOT 0 = 300

H.T.COEFF	STEAM TEMP	EMISSIVITY	RAD.WALL	SURFACE TEMP	OX/RET TEMP	FIX.HEATFLUX	CON.HEATFLUX	RAD.HEATFLUX	CON+RAD
0.0	0.0	0.0	0.0	885.54677	885.54677	0.0	0.0	0.0	0.0
0.10000	949.46444	0.0	0.0	885.54677	885.54677	0.0	6.43177	0.0	6.43177
O.PL.LIMIT	OXYGEN FLUX	C.IN OXIDE	O.IN ALPHA	O.IN BETA	OXYG.TOTAL	OXYG.GAIN	OXIDE LAYER	ALPHA LAYER	BETA LAYER
1.0000	0.0293	0.1378	0.0191	0.4148	0.5717	0.1549	0.9361	0.0003	484.5786

OUTSIDE OXIDE LAYER

POINT NUMBER = 1 2
 DISTANCE = -0.00003 0.00006
 TEMPERATURE = 885.55 885.55
 CONCENTRATION = 1.51400 1.43010

OUTSIDE ALPHA LAYER

POINT NUMBER = 2 2
 DISTANCE = 0.00006 0.00014
 TEMPERATURE = 885.55 885.55
 CONCENTRATION = 0.45365 0.02389

BETA LAYER

POINT NUMBER =	2	5	7	9	11	13	15	17	19	21	25	29	33
DISTANCE =	0.00014	0.00043	0.00064	0.00086	0.00107	0.00129	0.00150	0.00172	0.00193	0.00214	0.00246	0.01372	0.02050
TEMPERATURE =	885.55	885.55	885.55	885.55	885.55	885.55	885.55	885.55	885.55	885.55	885.55	885.55	885.55
CONCENTRATION =	0.00710	0.00633	0.00600	0.00587	0.00587	0.00593	0.00603	0.00613	0.00623	0.00630	0.00649	0.00649	0.00649

BETA LAYER

POINT NUMBER =	257	321	385	449	513	577	641
DISTANCE =	0.02744	0.03430	0.04116	0.04802	0.05488	0.06174	0.06860
TEMPERATURE =	885.55	885.55	885.55	885.55	885.55	885.55	885.55
CONCENTRATION =	0.00649	0.00649	0.00649	0.00649	0.00649	0.00649	0.00649

*** TIME = 30.000 ***

PLOT 0 = 300

H.T.COEFF	STEAM TEMP	EMISSIVITY	RAD.WALL	SURFACE TEMP	OX/RET TEMP	FIX.HEATFLUX	CON.HEATFLUX	RAD.HEATFLUX	CON+RAD
0.0	0.0	0.0	0.0	1269.57167	1269.57167	0.0	0.0	0.0	0.0
0.10000	1249.86772	0.0	0.0	1269.57167	1269.57167	0.0	-1.97040	0.0	-1.97040
O.PL.LIMIT	OXYGEN FLUX	O.IN OXIDE	O.IN ALPHA	O.IN BETA	OXYG.TOTAL	OXYG.GAIN	OXIDE LAYER	ALPHA LAYER	BETA LAYER
1.0000	0.2407	0.0429	0.2568	0.5344	1.6342	1.2140	5.7850	0.4913	672.6784

OUTSIDE OXIDE LAYER

POINT NUMBER = 1 5
 DISTANCE = -0.00019 0.00038
 TEMPERATURE = 1269.57 1269.57
 CONCENTRATION = 1.51400 1.40129

OUTSIDE ALPHA LAYER

POINT NUMBER = 5 13
DISTANCE = 0.00038 0.00123
TEMPERATURE = 1269.57 1269.57
CONCENTRATION = 0.45365 0.15210

BETA LAYER

POINT NUMBER = 13 15 17 19 21 23 25 27 29 31 33 35 37 39
DISTANCE = 0.00150 0.00172 0.00193 0.00214 0.00236 0.00257 0.00279 0.00300 0.00322 0.00344 0.00366 0.00388 0.00410 0.00432
TEMPERATURE = 1269.57 1269.57 1269.57 1269.57 1269.57 1269.57 1269.57 1269.57 1269.57 1269.57 1269.57 1269.57 1269.57 1269.57
CONCENTRATION = 0.04728 0.04431 0.04236 0.04033 0.03830 0.03631 0.03432 0.03230 0.03030 0.02830 0.02630 0.02430 0.02230 0.02030

BETA LAYER

POINT NUMBER = 257 321 385 449 513 577 641
DISTANCE = 0.02748 0.03430 0.04116 0.04802 0.05488 0.06174 0.06860
TEMPERATURE = 1269.57 1269.57 1269.57 1269.57 1269.57 1269.57 1269.57
CONCENTRATION = 0.00649 0.00649 0.00649 0.00649 0.00649 0.00649 0.00649

*** TIME = 35.000 ***

PLOT 0 = 314

Table with 10 columns: M.T.COEFF, STEAM TEMP, VISCOSITY, RAD.WALL SURFACE TEMP, OX/NET TEMP, FIX.HEATFLUX, CON.HEATFLUX, RAD.HEATFLUX, QCON/GRAD, O.PL.LIMIT, OXIGEN FLUX, O.IN OXIDE, O.IN ALPHA, O.IN BETA, OXID.TOTAL, OXID.GAIN, OXIDE LAYER, ALPHA LAYER, BETA LAYER.

OUTSIDE OXIDE LAYER

POINT NUMBER = 1 5 9
DISTANCE = -0.00043 0.00022 0.00084
TEMPERATURE = 1522.17 1522.17 1522.17
CONCENTRATION = 1.51400 1.44665 1.38235

OUTSIDE ALPHA LAYER

POINT NUMBER = 9 13 17 21 25 29 33
DISTANCE = 0.00084 0.00129 0.00172 0.00214 0.00257 0.00300 0.00341
TEMPERATURE = 1522.17 1522.17 1522.17 1522.17 1522.17 1522.17 1522.17
CONCENTRATION = 0.45365 0.40417 0.35729 0.31280 0.27004 0.23060 0.19476

BETA LAYER

POINT NUMBER = 33 41 49 57 65 73 81 89 97 105 113 121 129 137
DISTANCE = 0.00341 0.00429 0.00515 0.00600 0.00686 0.00772 0.00858 0.00943 0.01029 0.01115 0.01201 0.01287 0.01372 0.01458
TEMPERATURE = 1522.17 1522.17 1522.17 1522.17 1522.17 1522.17 1522.17 1522.17 1522.17 1522.17 1522.17 1522.17 1522.17 1522.17
CONCENTRATION = 0.09197 0.08239 0.07347 0.06543 0.05826 0.05188 0.04621 0.04114 0.03660 0.03268 0.02936 0.02664 0.02452 0.02299

BETA LAYER

POINT NUMBER = 257 321 385 449 513 577 641
DISTANCE = 0.02748 0.03430 0.04116 0.04802 0.05488 0.06174 0.06860
TEMPERATURE = 1522.17 1522.17 1522.17 1522.17 1522.17 1522.17 1522.17
CONCENTRATION = 0.00736 0.00665 0.00652 0.00649 0.00649 0.00649 0.00649

TABLE DA. SELECTED INPUT-OUTPUT FOR TEST CASE DA1 BURST-TEST WITH TEMPERATURE PROFILE CALCULATION.

ROST	0.3200	BALL	DOZIB(1)	SALPA(1)	DOZIB(2)	SALPA(2)
	0.04800	0.0	0.0	0.0	0.0	0.0
TRAX	0.0	STTRP	0.0	STTRP	2	MSRIFT
	0.0	0.0	5.0000	MSRIFT	1	MSRIFT
BLERS	0	MSRIB	0	MSRIB	1	MSRIB
	0	0	0	0	0	0
MSRIPP(H)	0.0	MSRIB(H)	0.0	MSRIB(H)	0.0	MSRIB(H)
	0.0	0.0	0.0	0.0	0.0	0.0
	0.0	0.1000	330.0000	0.0	0.0	0.0
MSRIPB(H)	0	MSRIPP(H)	0	MSRIPP(H)	0	MSRIPP(H)
	0	0	0	0	0	0
TRTART	0.004000	MSRIPP	0	MSRIPP	0	MSRIPP
	0.004000	0.0	0	0	0	0

*** MATERIAL PROPERTIES ***

METAL DENSITY	6.400	OXID DENSITY	5.020	GRM/CM ³	REACTION HEAT	30330.00	MBRC/GRAM OXIDEN
TEMP. (C)	STOCH. OX.	OXI/ALL	AL/STEA	DETA/AL	OXID	MSRIB	MSRIB
750.00	1.51400	1.40026	0.00016	0.00016	0.00000	0.19377	0.51785
800.00	1.51400	1.40031	0.00016	0.00016	0.00000	0.20752	0.53099
850.00	1.51400	1.40274	0.00016	0.00016	0.00000	0.22127	0.54423
900.00	1.51400	1.42901	0.00016	0.00016	0.00000	0.23502	0.55748
950.00	1.51400	1.47326	0.00016	0.00016	0.00000	0.24877	0.57072
1000.00	1.51400	1.51151	0.00016	0.00016	0.00000	0.26252	0.58397
1050.00	1.51400	1.51774	0.00016	0.00016	0.00000	0.27627	0.59721
1100.00	1.51400	1.51601	0.00016	0.00016	0.00000	0.29002	0.61046
1150.00	1.51400	1.51026	0.00016	0.00016	0.00000	0.30377	0.62370
1200.00	1.51400	1.50651	0.00016	0.00016	0.00000	0.31752	0.63695
1250.00	1.51400	1.50276	0.00016	0.00016	0.00000	0.33127	0.65019
1300.00	1.51400	1.50001	0.00016	0.00016	0.00000	0.34502	0.66344
1350.00	1.51400	1.50026	0.00016	0.00016	0.00000	0.35877	0.67668
1400.00	1.51400	1.50151	0.00016	0.00016	0.00000	0.37252	0.68993
1450.00	1.51400	1.50176	0.00016	0.00016	0.00000	0.38627	0.70317
1500.00	1.51400	1.50001	0.00016	0.00016	0.00000	0.40002	0.71642
1550.00	1.51400	1.50026	0.00016	0.00016	0.00000	0.41377	0.72966

• • • TIME = 20.000 • • •

PLOT 0 = 400

H.T.COEFF	STEAM TEMP	EMISSIVITY	RAD.WALL	SURFACE TEMP	OX/NET TEMP	FIX.HEATFLUX	CON.HEATFLUX	RAD.HEATFLUX	CON*GRAD
0.0	0.0	0.0	0.0	884.99547	884.99769	0.0	0.0	0.0	0.0
0.10000	949.27203	0.0	0.0	885.76602	885.76602	0.0	6.35060	0.0	6.35060
O.PL.LIMIT	OXYGEN FLUX	C.IN OXIDE	O.IN ALPHA	O.IN BETA	OXYG.TOTAL	OXYG.GAIN	OXIDE LAYER	ALPHA LAYER	BETA LAYER
1.0000	0.0293	0.1374	0.0190	0.4108	0.5712	0.1505	0.9335	0.7982	680.5025

OUTSIDE OXIDE LAYER

POINT NUMBER = 1 2
 DISTANCE = -0.00003 0.00006
 TEMPERATURE = 885.00 885.00
 CONCENTRATION = 1.51400 1.43014

OUTSIDE ALPHA LAYER

POINT NUMBER = 2 2
 DISTANCE = 0.00006 0.00014
 TEMPERATURE = 885.00 885.00
 CONCENTRATION = 0.45365 0.02365

BETA LAYER

POINT NUMBER	2	3	7	9	11	13	15	17	19	21	68	129	193
DISTANCE	0.00014	0.00043	0.00064	0.00086	0.00107	0.00129	0.00150	0.00172	0.00193	0.00214	0.00606	0.01372	0.02056
TEMPERATURE	885.00	885.00	885.00	884.99	884.99	884.99	884.99	884.99	884.99	884.99	884.99	884.99	885.00
CONCENTRATION	0.00705	0.00631	0.00599	0.00587	0.00587	0.00593	0.00603	0.00614	0.00623	0.00631	0.00649	0.00649	0.00649

BETA LAYER

POINT NUMBER	257	321	385	449	513	577	641
DISTANCE	0.02744	0.03030	0.04116	0.04802	0.05400	0.06174	0.06860
TEMPERATURE	885.04	885.11	885.19	885.30	885.43	885.59	885.77
CONCENTRATION	0.00649	0.00649	0.00649	0.00649	0.00649	0.00649	0.00649

• • • TIME = 30.000 • • •

PLOT 0 = 400

H.T.COEFF	STEAM TEMP	EMISSIVITY	RAD.WALL	SURFACE TEMP	OX/NET TEMP	FIX.HEATFLUX	CON.HEATFLUX	RAD.HEATFLUX	CON*GRAD
0.0	0.0	0.0	0.0	1270.00070	1270.02047	0.0	0.0	0.0	0.0
0.10000	1249.72037	0.0	0.0	1269.77106	1269.77106	0.0	-2.00507	0.0	-2.00507
O.PL.LIMIT	OXYGEN FLUX	C.IN OXIDE	O.IN ALPHA	O.IN BETA	OXYG.TOTAL	OXYG.GAIN	OXIDE LAYER	ALPHA LAYER	BETA LAYER
1.0000	0.2429	0.8443	0.2570	0.5352	1.6373	1.2175	5.7946	0.9209	673.6344

OUTSIDE OXIDE LAYER

POINT NUMBER = 1 5
 DISTANCE = -0.00020 0.00038
 TEMPERATURE = 1270.01 1270.02
 CONCENTRATION = 1.51400 1.40120

OUTSIDE ALPHA LAYER

POINT NUMBER = 5 13
 DISTANCE = 0.00038 0.00124
 TEMPERATURE = 1270.82 1270.80
 CONCENTRATION = 0.45365 0.15239

BETA LAYER

POINT NUMBER = 13 15 17 19 21 23 25 27 29 31 33 35 37 39 41
 DISTANCE = 0.00124 0.00150 0.00172 0.00193 0.00214 0.00236 0.00257 0.00279 0.00300 0.00322 0.00344 0.00366 0.00388 0.00410 0.00432
 TEMPERATURE = 1270.80 1270.79 1270.79 1270.78 1270.78 1270.77 1270.77 1270.76 1270.76 1270.75 1270.74 1270.73 1270.72 1270.71 1270.70
 CONCENTRATION = 0.04746 0.04473 0.04259 0.04054 0.03858 0.03670 0.03490 0.03318 0.03155 0.02998 0.02846 0.02698 0.02554 0.02414 0.02278

BETA LAYER

POINT NUMBER = 257 321 385 449 513 577 641
 DISTANCE = 0.02744 0.03430 0.04116 0.04802 0.05488 0.06174 0.06860
 TEMPERATURE = 1270.25 1270.14 1270.04 1269.95 1269.88 1269.82 1269.77
 CONCENTRATION = 0.00649 0.00649 0.00649 0.00649 0.00649 0.00649 0.00649

* * * * * TIME = 35.000 * * * * *

PLOT 0 = 414

U.T. CORR	STEAM TEMP	EMISSIVITY	RAD. WALL	SURFACE TEMP	OX/NET TEMP	FIX. HEAT FLUX	CON. HEAT FLUX	RAD. HEAT FLUX	QCON+QRAD
0.0	0.0	0.0	0.0	1524.46213	1524.51070	0.0	0.0	0.0	0.0
0.10000	1399.89815	0.0	0.0	1521.79352	1521.79352	0.0	-12.18954	0.0	-12.18954

O.FL. LIMIT	OXYGEN FLUX	C. IN OXIDE	O. IN ALPHA	O. IN BETA	OXYG. TOTAL	OXYG. GAIN	OXIDE LAYER	ALPHA LAYER	BETA LAYER
1.0000	0.6037	1.8472	0.8261	0.9288	3.6021	3.1738	12.7677	26.0563	851.4726

OUTSIDE OXIDE LAYER

POINT NUMBER = 1 5 9
 DISTANCE = -0.00043 0.00022 0.00085
 TEMPERATURE = 1524.46 1524.49 1524.51
 CONCENTRATION = 1.51400 1.44714 1.38217

OUTSIDE ALPHA LAYER

POINT NUMBER = 9 13 17 21 25 29 33
 DISTANCE = 0.00085 0.00124 0.00172 0.00214 0.00257 0.00300 0.00345
 TEMPERATURE = 1524.51 1524.49 1524.47 1524.45 1524.43 1524.40 1524.38
 CONCENTRATION = 0.45365 0.40568 0.35945 0.31518 0.27327 0.23430 0.19699

BETA LAYER

POINT NUMBER = 33 41 49 57 65 73 81 89 97 105 113 121 129 137
 DISTANCE = 0.00345 0.00429 0.00515 0.00600 0.00686 0.00772 0.00858 0.00943 0.01029 0.01115 0.01201 0.01287 0.01372 0.01458
 TEMPERATURE = 1524.38 1524.34 1524.26 1524.17 1524.08 1524.04 1523.99 1523.94 1523.89 1523.84 1523.79 1523.74 1523.69 1523.64
 CONCENTRATION = 0.09243 0.08337 0.07448 0.06645 0.05923 0.05277 0.04700 0.04183 0.03719 0.03300 0.02921 0.02574 0.02278 0.01980

BETA LAYER

POINT NUMBER = 257 321 385 449 513 577 641
 DISTANCE = 0.02744 0.03430 0.04116 0.04802 0.05488 0.06174 0.06860
 TEMPERATURE = 1523.28 1523.00 1522.73 1522.48 1522.23 1522.01 1521.79
 CONCENTRATION = 0.00740 0.00666 0.00652 0.00649 0.00649 0.00649 0.00649

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APPENDIX F
CODE LISTING - SIMSPAN 1

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C
ISH 0002 SIMSPAN 1
ISH 0003 IMPLICIT REAL*8 (A-H,O-S)
ISH 0004 NVALN PLO
ISH 0005 COMMON/RESULT/PLO(25,200), NPLOT, NPELOT
ISH 0006 COMMON/GEOMET/ R(1000), ROXID(2), RALFA(2), WALL, BOXID(2), DALFA(2), DR
1, DRUP(2)
ISH 0007 COMMON/TEMP/ T(1000), TOXID(2), TALFA(2), TSTART, TTEAM(2), TWALL(2)
ISH 0008 COMMON/HEAT/ HVER(100), HCOOL(2), HPRADIA(2), HRA(PL(2), OPINPR(2),
1, OSPLIT, HCAP(100), HSTAR(2), HPARIA(2)
2, OSURF(2), QCOM(2), QRAD(2), QREACT(2)
COMMON/HEADLN/ HITLE(20)
COMMON/CONCRW/ C(1000), COXID(2), COAL(2), CALSET(2), CBPTA(2),
1, OXIGL(2), NDIPP(2), CSTART, TAYN(2)
2, OCAP(500), OVEP(500), ODTMAX(500)
3, COA(2), CAO(2), CAB(2), CBA(2)
4, OCIPON(2), OCAPAO(2), OCAPAB(2), OCAPBA(2)
COMMON/ERIT / TIME, MAX, DTTEMP, DTDIPP, DTFRIM, DTMAX(100)
1, MTEMP, MDIPP, MPRINT
COMMON/MESS / MGRSS, MPINE, MOXID(2), MOXY(2)
1, NLUNB, MSTART, MALFA(2)
COMMON/MSHNT/ MT(100), MTCOOL(2), MWALL(2), MTCOOL(2), MWALL(2), MGRS
COMMON/MSHCO/ MC(500), MSHKEP, MGES, MCA(2), MAB(2)
1, MOA(2), MAO(2), MAB(2), MBA(2), INTOT(2), IMPB
2, MOA1, MAO1, MAB1, MAB1, MOXID1, MALFA1
3, MOA2, MAO2, MAB2, MAB2, MOXID2, MALFA2
COMMON/NATPRO/ DENZIR, DENHNO, OSTOCK, OXICO, GENHAT, PICFAC, OXHEAT
COMMON/PROPL/ CO(500), X(500), OLAYER(2), ALAYER(2), BLAYER, OOXID(2),
1, OALFA(2), OGAIN(2), OBETA, OSTOTAL, OBETAS, STRAP,
2, H2, H3, H4, H5, NUMBER, NSCALE
COMMON/HINPT/ NDIPPIN(100,2), TIMDIP(100,2), HCOEPP(100,2),
1, TCUEPP(100,2), HBRACO(100,2), TRADCO(100,2),
2, QFLUX(100,2), TQPLUX(100,2), TINSTP(100), DTHER(100),
3, NDIPPIN(2), NDIPPIN(2), FOPLEX(2), MOPLEX(2),
4, HCOEPP(2), HCOEPP(2), FRADCO(2), HBRACO(2), MSTEP
COMMON/POVAR/OLIMIT(2), CUNIT, PLOVIN
DIMENSION DOXLD(2), DALOLD(2)
C DXO = MAX. MOVEMENT OF OXIDE/ALPHA INTERFACE DURING 1 TIME STEP
C DXA = MAX. MOVEMENT OF ALPHA/BETA INTERFACE DURING 1 TIME STEP
C DTE = MAX. TEMPERATURE CHANGE DURING 1 TIME STEP
DIO=2, 3-6
DXA=5, 6-6
DTE=1.
DTE2=DDTY/2.
1 CALL INPUT
IF (M1).EQ.0.) GO TO 9999
R(1)=0. IS SET IN INPUT IF THERE IS NO NEXT CASE
CALL IADATA
INDATA PRINTS ALL INPUT DATA
MSTART=0
CALL INITIA
TEMP=-1.D-10
DIPR=-1.D-10
TPLOC=DTFRIMDFLOAT-1.D-10
TMATMAX=1.D-10

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15H 0035      TEMAX=DTTEMP
15H 0036      DTTEMP=DTDIFF
15H 0037      DELTA=DELTA+DELSIN*DELRAT
15H 0038      LSTEP=L
15H 0039      DOXOLD(1)=DOXID(1)
15H 0040      DOXOLD(2)=DOXID(2)
15H 0041      DALOLD(1)=DALFA(1)
15H 0042      DALOLD(2)=DALFA(2)
15H 0043      DOXOLD(1)=DOXID(1)+DOXID(2)
15H 0044      DOXOLD(2)=DOXID(2)
15H 0045      DOXOLD(1)=DOXID(1)
15H 0046      DOXOLD(2)=DOXID(2)
15H 0047      DOXOLD(1)=DOXID(1)
15H 0048      DOXOLD(2)=DOXID(2)
15H 0049      DOXOLD(1)=DOXID(1)
15H 0050      DOXOLD(2)=DOXID(2)
15H 0051      DOXOLD(1)=DOXID(1)
15H 0052      DOXOLD(2)=DOXID(2)
15H 0053      DOXOLD(1)=DOXID(1)
15H 0054      DOXOLD(2)=DOXID(2)
15H 0055      DOXOLD(1)=DOXID(1)
15H 0056      DOXOLD(2)=DOXID(2)
15H 0057      DOXOLD(1)=DOXID(1)
15H 0058      DOXOLD(2)=DOXID(2)
15H 0059      DOXOLD(1)=DOXID(1)
15H 0060      DOXOLD(2)=DOXID(2)
15H 0061      DOXOLD(1)=DOXID(1)
15H 0062      DOXOLD(2)=DOXID(2)
15H 0063      DOXOLD(1)=DOXID(1)
15H 0064      DOXOLD(2)=DOXID(2)
15H 0065      DOXOLD(1)=DOXID(1)
15H 0066      DOXOLD(2)=DOXID(2)
15H 0067      DOXOLD(1)=DOXID(1)
15H 0068      DOXOLD(2)=DOXID(2)
15H 0069      DOXOLD(1)=DOXID(1)
15H 0070      DOXOLD(2)=DOXID(2)
15H 0071      DOXOLD(1)=DOXID(1)
15H 0072      DOXOLD(2)=DOXID(2)
15H 0073      DOXOLD(1)=DOXID(1)
15H 0074      DOXOLD(2)=DOXID(2)
15H 0075      DOXOLD(1)=DOXID(1)
15H 0076      DOXOLD(2)=DOXID(2)
15H 0077      DOXOLD(1)=DOXID(1)
15H 0078      DOXOLD(2)=DOXID(2)
15H 0079      DOXOLD(1)=DOXID(1)
15H 0080      DOXOLD(2)=DOXID(2)
15H 0081      DOXOLD(1)=DOXID(1)
15H 0082      DOXOLD(2)=DOXID(2)
15H 0083      DOXOLD(1)=DOXID(1)
15H 0084      DOXOLD(2)=DOXID(2)
15H 0085      DOXOLD(1)=DOXID(1)
15H 0086      DOXOLD(2)=DOXID(2)
15H 0087      DOXOLD(1)=DOXID(1)
15H 0088      DOXOLD(2)=DOXID(2)
15H 0089      DOXOLD(1)=DOXID(1)
15H 0090      DOXOLD(2)=DOXID(2)
15H 0091      DOXOLD(1)=DOXID(1)
15H 0092      DOXOLD(2)=DOXID(2)
15H 0093      DOXOLD(1)=DOXID(1)
15H 0094      DOXOLD(2)=DOXID(2)
15H 0095      DOXOLD(1)=DOXID(1)
15H 0096      DOXOLD(2)=DOXID(2)
15H 0097      DOXOLD(1)=DOXID(1)
15H 0098      DOXOLD(2)=DOXID(2)

10      DTMIN=TIME-TIME+1.D-10
C      TIME STEP CONTROL (UP TO LABEL 140)
C      DTDIFF = TIME STEP FOR DISSIPATION CALCULATION
C      DTTEMP = TIME STEP FOR TEMPERATURE CALCULATION
      DTDIFF=DTTEMP
      DTTEMP=TEMAX
      DO 20 N=1,2
      IF(DIFF(N).EQ.0.) GO TO 20
      DT=DELTA/CHIGPL(N)
      IF(DT.GT.DTOLD) DT=1.03*DTOLD
      IF(DT.LT.DIPL) DTDIFF=DT
      DO=DABS(DOXID(N)-DOXOLD(N))
      DA=DABS(DALFA(N)-DALOLD(N))
      IF(DO.GT.DIPL) DTDIFF=DTOLD+DO/DO
      IF(DA.GT.DIPL) DTDIFF=DTOLD+DA/DA
      DOXOLD(N)=DOXID(N)
      DALOLD(N)=DALFA(N)
20      CONTINUE
      IF(DTDIFF.LT.DTMIN) DTMIN=DTDIFF
      IF(DTTEMP.LT.DTMIN) DTMIN=DTTEMP
      IF(FLURB.EQ.2) GO TO 70
      FLURB=2 NO TEMPERATURE CALCULATION
      DELTA=DABS(T(1)-TEND)
      IF(DELTA-DT(2) 50.50.60
50      DTTEMP=DTMIN
      GO TO 140
60      DTTEMP=DTOLD+DELTA/DELTA
      IF(DTTEMP.LT.DTMIN) DTMIN=DTTEMP
      GO TO 140
70      IF(MTCOOL(1).GT.0) GO TO 80
      MTCOOL(1) OR MTCOOL(2) GREATER THAN 0:
      TEMPERATURE IS FUNCTION OF TIME
      DTTEMP=TRAX
      GO TO 100
80      T(1)=TIMPM(MTCOOL(1),TCOOL,STCOOL,1,TIME)
      T(2)=TIMPM(MTCOOL(2),TCOOL,STCOOL,1,TIME)
      DELTA=DABS(T(1)-T(2))
      IF(DELTA.GT.1.) GO TO 90
      DTTEMP=PRINT-TIME
      GO TO 140
90      DTTEMP=(PRINT-TIME)/DELTA
      TTEMP-TIME
      GO TO 140
100      IF(MTCOOL(2).EQ.0) GO TO 140
      T(1)=TIMPM(MTCOOL(2),TCOOL,STCOOL,2,TIME)
      T(2)=TIMPM(MTCOOL(2),TCOOL,STCOOL,2,PRINT)

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158 0099      DELTA=DABS(T*HFIME)-TNEW)
158 0100      IP(DELTA,GT.1.) GO TO 120
158 0101      STEND=TPRINT-TIME
158 0102      GO TO 140
158 0103
158 0104      120 DTEND=(TPRINT-TIME)/DELTA
158 0105      TTEMP=TIME
158 0106      140 IP=DMIN.LT.DTIPP) DTIPP=D*MIN
158 0109      END OF TIME STEP CONTROL
158 0110      IP(TIME.LT.TEMP) GO TO 200
158 0111      DO 150 N=1,2
158 0112      IP(NCOOL(K),GT.0)ISTEAM(N)=TIMPUMINCOOL(N),TCOOL,STCOOL,4,TIME)
158 0113      IP(NWALL(N),GT.0)IWALL(N)=TIMPUMINWALL(N),T*ID,ST*ID,4,TIME)
158 0114      IP(NCORR(N),GT.0)NCOOL(N)=TIMPUMINCOOR(N),NCOORP,TCORPP,4,TIME)
158 0115      IP(NRADCO(N),GT.0)IRADIA(N)=TIMPUMINRADCO(N),NRADCO,TRADCO,4,TIME)
158 0116      IP(NMOLX(N),GT.0)QPIED(N)=TIMPUMINQPIUX(N),OPLUX,TOPLOX,4,TIME)
158 0117      CONTINUE
158 0118      TTHOLD=T(1)
158 0119      CALL TEPER
158 0120      T*MPX CALCULATES TEMPERATURES IN WALL
158 0121      TTEMP=TTEMP+DTEMP
158 0122      200 IP(TIME.LT.DIPP) GO TO 300
158 0123      N=NDIIPP(1)
158 0124      M=NDIPP(2)
158 0125      IP(MDIPIN(1),GT.0)MDIPP(1)=TIMPUM(MDIPIN(1),MDIPIN,TMDIP,1,TIME)
158 0126      IP(MDIPIN(2),GT.0)MDIPP(2)=TIMPUM(MDIPIN(2),MDIPIN,TMDIP,2,TIME)
158 0127      IP(MDIPP(1),LE.N1).AND.(MDIPP(2),LE.N2) NO TO 220
158 0128      D*DIPP=1.D-7
158 0129      D*MIN=1.D-7
158 0130      CALL DIPPUS
158 0131      DIPPUS CALCULATES OXYGEN PROFILE IN WALL
158 0132      IP(TIME,GT.0.) GO TO 250
158 0133      CALL OUTPUT
158 0134      OBTAS=OT*CAL
158 0135      250 TDIPP=TDIPP+DTDIPP
158 0136      300 TIME=TIME+DTIME
158 0137      DTOLD3=DTOLD2
158 0138      DTOLD2=DTOLD1
158 0139      DTOLD=DTIN
158 0140      IP(TIME.LT.TPRINT) GO TO 10
158 0141      DTOLD2=DTOLD3
158 0142      DTOLD=DTOLD2
158 0143      CALL OUTPUT
158 0144      OXYGEN - AND TEMPERATURE PROFILE ARE PRINTED
158 0145      IP(LSTEP,GT.NSTEP).OR.(TIME.LT.T*MS*P(LSTEP)-.000001)NO TO 400
158 0146      T*MPIN=D*MIN(LSTEP)
158 0147      DTMPW (LSTEP) IS THE NEW OUTPUT TIME STEP
158 0148      LSTEP=LSTEP+1
158 0149      TPRINT=TPRINT+DTPRIN
158 0150      IP(TIME.LT.TPLOT) GO TO 10
158 0151      T*PLOX=T*PLOX+DT*PRIN*DPLOAT:HPRINT)
158 0152      IP((NUMBER.EQ.0).OR.(NUMBER,GT.0)) GO TO 4010
158 0153      C*INIT=C*STAR
158 0154      PLOTIN=TIME
158 0155      OLIMIT(1)=MDIPP(1)
158 0156      OLIMIT(2)=MDIPP(2)
158 0157      STEMP=T(1)
158 0158      OXYGEN PROFILE IS PLOED
158 0159
158 0160
158 0161
158 0162
158 0163
158 0164
158 0165
158 0166
158 0167

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ISH 0168
ISH 0169
ISH 0170
ISH 0171
ISH 0172
ISH 0173
ISH 0174
ISH 0175
ISH 0176
ISH 0177
ISH 0178
ISH 0179

          CALL PROPLO
          NSCALE=NSCALE
          1.(NSCALE,RE.2) GO TO 1500
          NUMBER=NUMBER+1
          NSCALE=0
          CALL PROPLO
          NSCALE=2
          3500 NUMBER=NUMBER+1
          4000 IF(TIME.LT.TMAX) GO TO 10
          IPINPLOT .GT.0) CALL TRAPLO
          C TRAPLO PLOTS UP TO 24 VARIABLES AS FUNCTIONS OF TIME OF SQUARE
          C ROOT OF TIME
          GO TO 1
          9999 IPINNUMBER,10.0) STOP
          NUMBER=NUMBER
          CALL PROPLO
          STOP
          END

ISH 0181
ISH 0182
ISH 0184
ISH 0185
ISH 0186
ISH 0187

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ISN 0002      SUBROUTINE INPUT
ISN 0003      C ALL INPUT DATA ARE READ IN THIS SUBROUTINE
ISN 0004      IMPLICIT REAL*8 (A-H,O-Z)
ISN 0005      REAL*8 PLO
ISN 0006      COMMON/RESULT/PLO(25,200), NPLOT, NPLOT
ISN 0007      COMMON/CONST/ P (1000), RCOXD (2), RALPA (2), WALL, DOXID (2), DALPA (2), DP
ISN 0008      COMMON/TEMP / T (1000), TOXID (2), TALPA (2), TSTART, TSTEP (2), TWALL (2)
ISN 0009      1, TSHRP (2)
ISN 0010      COMMON/TEMPIN/ TCOOL (100,2), STCOOL (100,2), TRAD (100,2), TTPAD (100,2)
ISN 0011      COMMON/HEAT / HVEP (100), HCOOL (2), FRACIA (2), HEATFL (2), QPIXFD (2),
ISN 0012      1 QSPLOT, HCAP (100), HSTEAM (2), HRADIA (2)
ISN 0013      2 QSURF (2), UCON (2), QRAD (2), QREACT (2)
ISN 0014      COMMON/HEADIN/ NTITLE (30)
ISN 0015      COMMON/CONCEN/ C (1000), COXID (2), COXAL (2), CALDPT (2), CRTPA (2),
ISN 0016      1 OXIGPL (2), HDIIP (2), CSTART, NATN (2)
ISN 0017      2, HCAP (500), OVER (500), ODTMAX (500)
ISN 0018      3, COA (2), CAO (2), CABI (2), CBAI (2)
ISN 0019      4, OCAPOA (2), OCAPAO (2), OCAPAB (2), OCAPBA (2)
ISN 0020      COMMON/EXIT / TIME, THAX, DTTENP, DTDIFF, DTPRN, DTMAX (100)
ISN 0021      1, NTERP, NDIFP, NPRIHT
ISN 0022      COMMON/MESS / NGRDSS, NFINR, ROXID (2), HOXI (2)
ISN 0023      1, WLWB, NSTART, NALPA (2)
ISN 0024      COMMON/MESSNTE/NT (100), NTCOOL (2), NTWALL (2), NTCOOL (2), NTWALL (2), NGRS
ISN 0025      COMMON/MESSCO/NC (500), NBAKER, NGRS, NOA (2), NAB (2)
ISN 0026      1, NOA (2), NAO (2), NAB (2), NBA (2), INTOXI (2), INTB
ISN 0027      2, NOA1, NAO1, NAB1, NBA1, NOXD1, NALPA 1
ISN 0028      3, NOA2, NAO2, NAB2, NBA2, NOXD2, NALPA 2
ISN 0029      COMMON/NATPRO/ DENR, DENR2, OSTOCH, OYTCO, DENRAT, PICFAC, OHEAT
ISN 0030      COMMON/PROPIL/ CO (500), X (500), OLAYER (2), ALAYER (2), BLAYER, OOXID (2),
ISN 0031      1 OALPA (2), OGAIN (2), OBETA, OTOTAL, OBETAS, STCRP,
ISN 0032      2N1, N2, N3, N4, N5, NUMBER, NSCALE
ISN 0033      COMMON/INPUT/ HDIFIN (100,2), TINDIP (100,2), HCOEFP (100,2),
ISN 0034      1 TCOEFP (100,2), HRADCO (100,2), TRADCO (100,2),
ISN 0035      2 QFLUXI (100,2), TOPLUX (100,2), TINSTP (100), DTNEV (100),
ISN 0036      3 HDIFIN (2), HDIFIN (2), KOPIUX (2), HOPLUX (2),
ISN 0037      4 HCOEFP (2), HCOEFP (2), HRADCO (2), HRADCO (2), NSTEP
ISN 0038      4=5
ISN 0039      READ (N, 150, END 1001) (NTITLE(K), K=1, 20)
ISN 0040      150 FORMAT (20A8)
ISN 0041      READ (N, 200) R (1), WALL, OLAYER (1), ALAYER (1), CLAYER (2), ALAYER (2)
ISN 0042      200 FORMAT (8D10.9)
ISN 0043      READ (N, 250) THAX, DTTENP, DTDIFF, DTPRN, NSTEP, NPRIHT, NUMBER, NSCALE
ISN 0044      250 FORMAT (8D10.9, 4I10)
ISN 0045      IF (NSTEP.GT.0) READ (N, 200) (TINSTEP(K), DTNEV(K), K=1, NSTEP)
ISN 0046      READ (N, 400) WLWB, NBAKER
ISN 0047      READ (N, 300) (NDIFP(K), HCOOL(K), TSTEP(K), HRADIA(K), TWALL(K),
ISN 0048      1 QPIXFD(K), K=1, 2)
ISN 0049      300 FORMAT (6D10.9)
ISN 0050      READ (N, 400) (HDIFIN(K), HCOEFP(K), NTCOOL(K), HRADCO(K), NTWALL(K),
ISN 0051      1 HOPLUX(K), K=1, 2)
ISN 0052      400 FORMAT (6I10)
ISN 0053      DO 100 K=1, 2
ISN 0054      IF (HDIFIN(K).EQ.0) GO TO 20
ISN 0055      N=HDIFIN(K)
ISN 0056      READ (N, 200) (NDIFIN(L,K), TINDIP(L,K), L=1, N)
ISN 0057      20 IF (HCOEFP(K).EQ.0) GO TO 30

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ISH 0040      M=MCORPP(N)
ISH 0041      READ(N,200) (MCORPP(L,K),TCORPP(L,K),L=1,M)
ISH 0042      TP:MTCCOOL(N),TQ:0) GO TO 40
ISH 0043      M=MTCCOOL(N)
ISH 0044      READ(N,200) (TCOOL(L,K),STCOOL(L,K),L=1,M)
ISH 0045      TP:MRADCO(N),TQ:0) GO TO 50
ISH 0046      M=MRADCO(N)
ISH 0047      READ(N,200) (MRADCO(L,K),TRADCO(L,K),L=1,M)
ISH 0048      TP:MTWALL(N),TQ:0) GO TO 60
ISH 0049      M=MTWALL(N)
ISH 0050      READ(N,200) (TRAD(L,K),STRAD(L,K),L=1,M)
ISH 0051      TP:MPLOX(N),TQ:0) GO TO 100
ISH 0052      M=MPLOX(N)
ISH 0053      READ(N,200) (PFLX(L,K),TOPFLX(L,K),L=1,M)
ISH 0054      100 CONTINUE
ISH 0055      TSTART,CSTART,OSPLIT,DUMY,NDUMY1,NDUMY2,NDUMY3,MPLOT
ISH 0056      RETURN
ISH 0057      1001 P(1)=0.
ISH 0058      RETURN
ISH 0059      END
ISH 0060
ISH 0061
ISH 0062
ISH 0063

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15W 0002 SUBROUTINE IMDATA
15W 0003 YDATA PRINTS ALL INPUT DATA
15W 0004 IMPLICIT REAL*8 (A-H,O-Z)
15W 0005 REAL*8 PLC
15W 0006 COMMON/RES/PL0(25,200),MPLOT,MPLCT
15W 0007 COMMON/GRDSET/ R(1000),ROTX(2),RALFA(2),WALL,MXID(2),DALFA(2),DR
15W 0008 COMMON/TEMP / T(1000),TOXID(2),TALPA(2),TSTART,TTEAM(2),TWALL(2)
15W 0009 ,TSURP(2)
15W 0010 COMMON/TEMPIN/ TCOOL(100,2),MCOOL(100,2),TRAD(100,2),STRAD(100,2)
15W 0011 COMMON/HEAT / HVER(100),MCCOL(2),EPADIA(2),HRADPL(2),QFINED(2),
15W 0012 OSPLIT,HCAP(100),MTEAM(2),HRADIA(2)
15W 0013 ,QSURP(2),OCOM(2),QVAR(2),QREACT(2)
15W 0014 COMMON/HEADIN/ HITLE(20)
15W 0015 COMMON/CONCEN/ C(1000),COXID(2),CONAL(2),CALSP(2),CBETA(2),
15W 0016 ,OCAP(500),OZER(500),ODTMAX(100)
15W 0017 ,COA(2),CAO(2),CAB(2),CBA(2)
15W 0018 ,OCAPOA(2),OCAPO(2),OCAPAR(2),OCAPAR(2)
15W 0019 COMMON/EBIT / TIME,THAX,DTTRP,DTDIPP,DTPRIN,DTYAK(100)
15W 0020 ,MTEMP,MNDIPP,MFINIT
15W 0021 COMMON/RESH /MGRSS,MPIRP,MOXID(2),MOXI(2)
15W 0022 ,MLUMB,MSTART,MALPA(2)
15W 0023 COMMON/RESKTE/NT(100),MCOOL(2),MFWALL(2),MCOOL(2),MFWALL(2),MGRS
15W 0024 COMMON/RESMCO/MC(500),MBAKER,MGRS,MCA(2),MAB(2)
15W 0025 ,MOR(2),MRO(2),MBA(2),MBA(2),MBA(2),MTOXI(2),MNB
15W 0026 ,MOR1,MOR2,MOR3,MOR4,MOR5,MOR6,MOR7,MOR8,MOR9,MOR10
15W 0027 ,MOR11,MOR12,MOR13,MOR14,MOR15,MOR16,MOR17,MOR18,MOR19,MOR20
15W 0028 COMMON/MATPRO/ DENSI,DEMO,OSTOCH,CHICOR,DEBRAS,DECPAC,OHHEAT
15W 0029 COMMON/PROPL/ CO(500),X(500),OLAYR(2),ALAYR(2),BLAYR,COXID(2),
15W 0030 ,MCOEPP(2),MCTPP(2),MFRADCO(2),MFRADCO(2),MSTEP
15W 0031 ,J=6
15W 0032 MSTR(J,500) (MTITLE(K),K=1,20)
15W 0033 MFORMAT(1),25,208//)
15W 0034 MSTR(J,599)
15W 0035 MFORMAT(10)0
15W 0036 ,110H DOXID(2),10H DALPA(2)
15W 0037 MSTR(J,600) R(1),WALL,OLAYR(1),ALAYR(1),OLAYR(2),ALAYR(2)
15W 0038 MFORMAT(10)10,4)
15W 0039 MSTR(J,650)
15W 0040 ,65C MFORMAT(10)0
15W 0041 ,THAX,10H DTTRP,10H DTDIPP,10H DTPRIN,
15W 0042 ,MTEMP,10H MPRINT,10H NUMBER,10H MSCALE
15W 0043 MSTR(J,660) THAX,DTTRP,DTDIPP,DTPRIN,MSTEP,MPRINT,NUMBER,MSCALE
15W 0044 MFORMAT(10)0,0,0,0,0)
15W 0045 MSTR(J,798)
15W 0046 ,798 MFORMAT(10)0
15W 0047 ,MLUMB,10H MBAKER
15W 0048 ,MTEMP,10H MPRINT,10H MSCALE
15W 0049 MSTR(J,498)
15W 0050 ,MFORMAT(10)0
15W 0051 ,MCOOL(K),10H MTEAM(K),10H EPADIA(K),
15W 0052 ,TWALL(K),10H QFINED(K)
15W 0053 MSTR(J,700) MNDIPP(K),MCOOL(K),MTEAM(K),TTEAM(K),HRADIA(K),

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ISM 0034
ISM 0037
ISM 003A
ISM 0039
ISM 0040
ISM 0041
ISM 0042
ISM 0043
ISM 0044
ISM 0045
ISM 0046

1
700 FORMAT (P10.4)
WRITE(J,700)
799 FORMAT (10HNDIPIR(K),10H HCOEPI(K),10H HTCOL(K),
10H HADCO(K),10H HWALL(K),10H HOPUE(K),
10H HADCO(K),10H HCOEPI(K),10H HTCOL(K),10H HADCO(K),10H HWALL(K),
10H HOPUE(K),K=1,2)
800 FORMAT (6I10)
WRITE(J,800)
699 FORMAT (10H0 TSTART,10H CSTART,10H QSPLOT,45X,5HPLOT)
WRITE(J,750) TSTART,CSTART,QSPLOT,HPLOT
750 FORMAT (P10.2,P10.6, P10.2, 40X,I10////)
STOP
END

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ISN 0002      SUBPONTYNT MATMAP
C             A TABLE WITH ALL MATERIAL PROPERTIES IS CALCULATED AND PRINTED
ISN 0003      EXPLICIT REAL*8 (A-H,O-Z)
ISN 0004      COMMON/HEADLN/ NTITLE(20)
ISN 0005      COMMON/MATPRO/ DENZIR,DENZRO,OSTOCH,OXICOM,DENRAT,PICPAC,OXHEAT
ISN 0006      J=6
ISN 0007      WRITE(J,10)
ISN 0008      10 FORMAT(1H0//47X,35H * * * MATERIAL PROPERTIES * * * ,//)
ISN 0009      WRITE(J,20) DENZIR,DENZRO,OXHEAT
ISN 0010      20 FORMAT(1H0,15HMETAL DENSITY = ,P7.3,5X,14HMOXID DENSITY = ,P7.3,5X,
1              10HGRAM/CM**3 ,10X,15HREACTION HEAT = ,P10.2,3X,
2              14HJESRC/GRAM OXYGEN )
ISN 0011      WRITE(J,30)
ISN 0012      30 FORMAT:1H0/20X,40HEQUILIBRIUM CONCENTRATION (GRAM/CM**3) ,2X,
13HDIFFUSION CONSTANT (CM**2/SEC) ,1X,16HTECHONDUCTIV(CM**C) ,1X,
22HNSP. HEAT M*SEC/(GR.C) )
ISN 0013      WRITE(J,40)
ISN 0014      40 FORMAT:1H0,10H TEMP. (C) ,10H STOCH. OX. ,10H OX./AL. ,10H AL./OX.
1,              10H AL./BETA ,10H BETA/AL. ,10H OXID ,10H ALPHA
2,              10H BETA ,10H OXID ,10H METAL ,10H OXID
3,              10H METAL )
ISN 0015      T=750.
ISN 0016      DO 140 I=1,17
ISN 0017      CALL INTPAC(T,CORAL,CALOX,1)
ISN 0018      CALL INTPAC(T,CALBE,CBEAL,2)
ISN 0019      DOX= DIFCON(T,OXICOM,CORAL,1)*PICPAC**2
ISN 0020      CORAL=CORAL/PICPAC
ISN 0021      DAL= DIFCON(T,CALOX,CALBE,2)
ISN 0022      DBE= DIFCON(T,CBEAL,C,3)
ISN 0023      TNCORO=CONDC(T,T,1)*PICPAC
ISN 0024      TNCORR=CONDC(T,T,2)
ISN 0025      SPHEOX=SPEC(T,1)/(PICPAC*DENZRO)
ISN 0026      SPHENE=SPEC(T,2)/DENZIR
ISN 0027      WRITE(J,50) T,OSTOCH,CORAL,CALOX,CALBE,CBEAL,DOX,DAL,DBE,
1              TNCORO,TNCORR,SPHEOX,SPHENE
ISN 0028      50 FORMAT:1H ,P10.2,5P10.5,3D10.3,4P10.4)
ISN 0029      T=T+50.
ISN 0030      100 CONTINUE
ISN 0031      WRITE(J,500) (NTITLE(K),K=1,20)
ISN 0032      500 FORMAT(1H1,25X,20A//)
ISN 0033      RETURN
ISN 0034      END

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15H 0002      SUBROUTINE INITIA
15H 0003      INITIA SETS THE INITIAL CONDITIONS
15H 0004      IMPLICIT REAL*8 (A-H,O-S)
15H 0005      REAL*8 PLO
15H 0006      COMMON/RESULT/ PLO(25,200), NPLOT, MPLOY
15H 0007      COMMON/GEOMNT/ R(1000), BOXID(2), PALPA(2), WALL, DOT'D(2), DALPA(2), DR
15H 0008      COMMON/TEMP / T(1000), TOXID(2), CALPA(2), TSTART, TSTEAM(2), TWALL(2)
15H 0009      1, TSTOP(2)
15H 0010      COMMON/TEMPIN/ TCOOL(100,2), STCOOL(100,2), TRAD(100,2), ETRAD(100,2)
15H 0011      COMMON/HEAT / HVER(100), HCOOL(2), PRADIA(2), HEATPL(2), HTRAD(2),
15H 0012      1, QSPILT, HCAP(100), HSTEAM(2), HRADIA(2)
15H 0013      2, OSBRP(2), UCOR(2), OPAD(2), OORACT(2)
15H 0014      COMMON/HEADLW/ HTITLE(20)
15H 0015      COMMON/CONCRN/ C(1000), COXID(2), COXAL(2), CALRET(2), CBETA(2),
15H 0016      1, OZIGPL(2), HZIPP(2), CSTART, OAZM(2)
15H 0017      2, OCAP(500), OOVER(500), ODTMAX(500)
15H 0018      3, COA(2), CAD(2), CAB(2), CBA(2)
15H 0019      4, OCAPOL(2), OCAPAO(2), OCAPAB(2), OCAPBA(2)
15H 0020      COMMON/SEIT / TIME, THA, DTTEMP, DTDIPP, DTPRM, DTHAX(100)
15H 0021      1, MTEMP, MDIPP, MPDIPP
15H 0022      COMMON/MESH / MGROSS, MFINE, MOXID(2), MOXI(2)
15H 0023      1, MLDNR, MSTART, MALPA(2)
15H 0024      COMMON/MESHTE/ WT(100), WCOOL(2), MFWALL(2), MTCOOL(2), MTWALL(2), MGRS
15H 0025      COMMON/MESHCO/ C(500), MRAKER, MRES, MOXI(2), MAB(2)
15H 0026      1, MOA(2), MAO(2), MAB(2), MAA(2), MAA(2), INTOXI(2), INTB
15H 0027      2, MOA1, MAO1, MAB1, MAA1, MOXID1, MALPA1
15H 0028      3, MOA2, MAO2, MAB2, MAA2, MOXID2, MALPA2
15H 0029      COMMON/MATPRO/ DENH2, DENH2O, OSTOCH, OXICOH, DEMRAT, PICPAC, CHEZAT
15H 0030      COMMON/PROPL/ CO(500), X(500), OLATEP(2), ALAYER(2), BLAYER, OOXID(2),
15H 0031      1, OALPA(2), OGAIN(2), OBEA, OTOCAL, OBEA3, STEPP,
15H 0032      2, M1, M2, M3, M4, M5, NUMBER, NSCALE
15H 0033      COMMON/INIPUT/ NDIPP(100,2), TNDIPP(100,2), HCOEPP(100,2),
15H 0034      1, TCOEPP(100,2), HRAJCO(100,2), TRADCO(100,2),
15H 0035      2, QPLUX(100,2), TQPLUX(100,2), TINSTE(100), PCHMVB(100),
15H 0036      3, MDIPP(2), MDIPPIN(2), MOPLUX(2), MOPLUX(2),
15H 0037      4, HCOEPP(2), HCOEPP(2), HRAJCO(2), HRAJCO(2), MSTEP
15H 0038      DENH2=6.49
15H 0039      DENH2O=5.82
15H 0040      OSTOCH=1.516
15H 0041      DEMRAT=OSTOCH/ (DENH2O-OSTOCH)
15H 0042      PICPAC=DEMTR/ (DENH2O-OSTOCH)
15H 0043      OXICOH=OSTOCH*PICPAC
15H 0044      ORHEAT=34330.
15H 0045      TINY=0.
15H 0046      KPILOT=0
15H 0047      IPIDTEMP, EQ=0.) DTEMP=DTDIPP
15H 0048      IPIDTIPP, EQ=0.) DTDIPP=DTDIPP
15H 0049      MGROSS=WALL/ .0064
15H 0050      MFINE=MGROSS
15H 0051      KPIPR=MPIN
15H 0052      DR=WALL/MPINE
15H 0053      MRES=MGROSS*.1
15H 0054      MPIN=MPINE*.1
15H 0055      T(1)=TSTART
15H 0056      C(1)=CSTART
15H 0057      DO 10 N=2, MPINE

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ISM 0109
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ISM 0152
ISM 0153
ISM 0154

1: TVAL(L,K)+273.16)*0.001-ITSTART+273.16)*0.001
HEATFL(R)=QCON(R)*GRAD(R)
30 CONTINUE
IF (NDIPP(1).EQ.0.) OR. (NBARR.GT.0) GO TO 40
C(1)=OXICO
SLOPE=C(1)*CVA(1)/DOXID(1)
OXIGFL(1)=SLOPE*DIPCON(T(1),TOXID(1),C(1),COA(1),1)
IF (DOXID(1).LT.4.*DBL.OR. (DALFA(1)-DOXID(1).LT.6.*DBL) GO TO 40
NR=NOXID(1)
DO 31 L=2,NR
31 C(L)=C(L-1)*SLOPE*DR
NL=NL+1
SLOPE=CAO(1)-CAB(1)/(NOXID(1)-RALFA(1))
C(NL)=CAO(1)-NOXID(1)-R*(NL)*SLOPE
NR=RALFA(1)
NL=NL+1
DO 32 L=NL,NR
32 C(L)=C(L-1)*SLOPE*DR
40 IF (NDIPP(2).EQ.0.) OR. (NBARR.GT.0) GO TO 50
C(NPIME)=OXICO
SLOPE=C(NPIME)-COA(2)/(NOXID(2))
OXIGFL(2)=SLOPE*DIPCON(T(NPIME),TOXID(2),C(NPIME),COA(2),1)
IF (DOXID(2).LT.4.*DBL.OR. (DALFA(2)-DOXID(2).LT.6.*DBL) GO TO 50
NR=NPIME-1
NR=NOXID(2)
C(NL)=C(NPIME)-SLOPE*(R(NL)-R(NPIME))
NL=NL+1
DO 41 L=NL,NR
41 C(L)=C(L-1)*SLOPE*DR
NR=NPIME-NOXID(2)-1
NL=NPIME-RALFA(2)
SLOPE=CAO(2)-CAB(2)/(RALFA(2)-DOXID(2))
C(NL)=CAO(2)-R(NL)-NOXID(2)*SLOPE
C(NL)=CAO(2)-R(NL)*SLOPE
NR=NR-1
NL=NL+1
DO 42 L=NL,NR
42 C(L)=C(L-1)*SLOPE*DR
50 CALL MATMAY
IF (NBARR.GT.0) CALL MATMAY
RETURN
END

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C
15W 0002 SUBROUTINE TEMPER
15W 0003 TEMPR CALCULATES THE TEMPERATURES IN THE WALL
15W 0004 IMPLICIT REAL*8 (A-H,O-Z)
15W 0005 COMMON/GEOMETRY/ R(1000),ROXID(2),RALPA(2),WALL,DOXID(2),DALPA(2),DR
15W 0006 / T(1000),TOXID(2),TALPA(2),TSTAR,T,STEAM(2),TWALL(2)
15W 0007 / TSNRP(2)
15W 0008 COMMON/TSTART/ TCOOL(100,2),T*COOL(100,2),TRAP(100,2),STRAD(100,2)
15W 0009 / HVER(100),HCOOL(2),FRADIA(2),HFA*PL(2),OPLIN(2),
15W 0010 / OSPLIT,H*CAP(100),H*STEAM(2),H*RADIA(2)
15W 0011 / OSURP(2),OCOM(2),ORAD(2),OPEACT(2)
15W 0012 / WITTL(20)
15W 0013 COMMON/MZADLA/ C(1000),COXID(2),COAL(2),CALBET(2),CBETA(2),
15W 0014 / ORIGPL(2),NDIPP(2),CSTART,GAIN(2)
15W 0015 / OCAT(500),OVER(500),ODTMAX(500)
15W 0016 / COA(2),CAO(2),CAB(2),CBA(2)
15W 0017 / OCARPOA(2),OCARPO(2),OCARPA(2),OCAPBA(2)
15W 0018 COMMON/EXIT / TIME,THAX,DTTEMP,DTDIPP,DTPRIN,DTMAX(100)
15W 0019 / VFF*,NDIPP,HEPINT
15W 0020 COMMON/RESR /H*GROSS,H*PIPE,WOXID(2),HOXI(2)
15W 0021 / H*UFB,H*STAR,HALPA(2)
15W 0022 COMMON/RESRTA/NT(100),H*COOL(2),H*WALL(2),H*TCOOL(2),H*WALL(2),H*RES
15W 0023 /H*HCO/HC(500),H*BAKER,H*GES,H*OA(2),HAB(2)
15W 0024 /H*AC(2),H*AC(2),H*AB(2),H*BA(2),H*TOXI(2),H*INTB
15W 0025 /H*AO1,H*AO1,H*AB1,H*BA1,HOXID1,HALPA1
15W 0026 /H*AO2,H*AO2,H*AB2,H*BA2,HOXID2,HALPA2
15W 0027 COMMON/HATPRO/ DENSI,DENSO,OSTOCH,OXICOH,DEHAT,PICTAC,ORHEAT
15W 0028 /CO(500),X(500),OLAYER(2),ALAYER(2),BLAYER,COXID(2),
15W 0029 /OALPA(2),OBAIN(2),OBETA,OT*AL,OBETA5,ST*EMP,
15W 0030 /H1,H2,H3,H4,H5,NUMBER,NSCALE
15W 0031 COMMON/HATPRO/ NDIPP(100,2),T*MDIP(100,2),H*CORPP(100,2),
15W 0032 /TCOEP(100,2),H*ADCO(100,2),H*TRADCO(100,2),
15W 0033 /QZOXI(100,2),TOPLUX(100,2),T*INSTR(100),DTNEW(100),
15W 0034 /KDIPIR(2),H*DIPIR(2),H*QPLUX(2),H*QPLUX(2),
15W 0035 /H*CORPP(2),H*ADCO(2),H*ADCO(2),H*STRP
15W 0036 DIMENSION HVER(1:2),H*SI(2:2),TR(1000),HOXI(2),M*TR(2)
15W 0037 /H*CORPP(2),H*ADCO(2),H*ADCO(2)
15W 0038 /TSURK(1)=T(1)+273.15
15W 0039 /TSURK(2)=T(M*TR)+273.15
15W 0040 H*GES=H*GROSS
15W 0041 /H*OXID(1)=H(1)-DOXID(1)
15W 0042 /H*OXID(2)=H(M*TR)-DOXID(2)
15W 0043 /H*SURP(1)=H(1)
15W 0044 /H*SURP(2)=H(M*TR)
15W 0045 DO 10 K=1,2
15W 0046 IF(NDIPP(K).EQ.0.) GO TO 5
15W 0047 /H*OXID(K)=DOXID(K)/DR*.5
15W 0048 /H*OXI(K)=HOXI(K)/16
15W 0049 /H*GES=H*GES+HOXID(K)/16+H*OXI(K)/32+H*OXID(K)/64
15W 0050 /H*(H*UFB+H*UFB*.67) H*GES=1
15W 0051 IF(H*COOL(K).GT.0.) H*STEAM(K)=H*COOL(K)*H*SURP(K)
15W 0052 /H*FRADIA(K)=H*O*.5 GO TO 10
15W 0053 /H*WALL(K)+273.15
15W 0054 /H*FRADIA(K)=BRADIA(K)+5.77E-12*(TSURK(K)+2)*T**2
15W 0055 /OSURP(K)
15W 0056 10 CONTINUE
15W 0057 M*(1)=1

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ISW 0042      NVER(1)=NSTRAN(1)+NRADIA(1)
ISW 0043      NVER(NGES+1)=NSTRAN(2)+NRADIA(2)
C            TLUWB = 0: TEMPERATURE PROFIL IS CALCULATED
C            TLUWB = 1: UNIFORM WALL TEMPERATURE IS CALCULATED
C            TLUWB = 2: WALL TEMPERATURE IS INPUT
IF(TLUWB.EQ.0) GO TO 18
CALL TLUWB
GO TO 2000
18 NT(NGES)=NPFINE
IF(NDIFF(1).GT.0.) GO TO 20
NCAP(1)=32.*DR*R(17)*SPEC(T(1),2)
NROUT=2
GO TO 190
20 NOXI(1)=NOXI(1)+1
IF(NOXI(1).GT.1) GO TO 30
NEAN=(2+NOXID(1))/2
NOXI(1)=R;NEAN)/DOXID(1)*CONDC(T(1),T;NOXID(1)+1),1)
NEAN2=(NOXID(1)+34)/2
NCAP(1)=R;NEAN)*DOXID(1)*SPEC(TOXID(1),1)
1 +R;NEAN2)*ROXID(1)-P(33))*SPEC(TOXID(1),2)
NT(2)=65
NEAN2=(NOXID(1)+66)/2
NEIR(1)=R;NEAN2)/ROXID(1)-R(65))*CONDC(TOXID(1),T(65),2)
NVER(2)=NEIR(1)*NOXI(1)/(NEIR(1)+NOXI(1))
NCAP(2)=R(65)*64.*DR*SPEC(T(65),2)
NROUT=3
GO TO 100
30 NCAP(1)=8.*DR*R(5)*SPEC(T(1),1)
NT(NOXI(1))=NOXID(1)+1
T(NT;NOXI(1))=TOXID(1)
NOXOUT=NOXI(1)-1
IF(NOXOUT.LT.2) GO TO 50
DO 40 K=2,NOXOUT
NT(K)=NT(K-1)+16
NT=NT(K)
NCAP(K)=16.*DR*B(NT)*SPEC(T(NT),1)
NVER(K)=R;NT-8)/16.*DR)*CONDC(T(NT),T(NT-16),1)
40 CONTINUE
50 NT;NOXI(1)+1)=NT;NOXI(1))+95)/64*64+1
NEAN=(NT(NOXOUT)+NT;NOXI(1)))/2
NVER(NOXI(1))=R;NEAN)/R(NT(NOXOUT))-ROXID(1))
1 *CONDC(T(NT(NOXOUT)),TOXID(1),1)
NEAN2=(NT(NOXI(1)+1)-32+NT(NOXI(1)))/2
NEAN0=NT;NOXOUT)+8+NT(NOXI(1)))/2
NCAP;NOXI(1))=R;NEAN0)*R;NT;NOXOUT)+8)-ROXID(1))*SPEC(TOXID(1),1)
1 +R;NEAN2)*ROXID(1)-R(NT(NOXI(1)+1)-32))*SPEC(TOXID(1),2)
NEAN=NT;NOXOUT)+16+NT;NOXI(1)))/2
NOXI(1)=R;NEAN)/R;NT;NOXOUT)+16)-ROXID(1))
1 *CONDC(T(NT(NOXOUT)+16),TOXID(1))
N1=NOXI(1)+1
NT=NT(N1)
NEAN2=NT;NOXI(1)+NT)/2
NVER(N1)=R;NEAN2)/ROXID(1)-R(NT))*CONDC(TOXID(1),T(N1),2)
NCAP(N1)=64.*DR*B(NT)*SPEC(T(N1),2)
NROUT=NOXI(1)+2
100 IF(NDIFF(2).GT.0.) GO TO 120
NCAP(NGES)=32.*DR*R(NFINE-16)*SPEC(T(NFINE),2)
NVER(NGES)=R;NFINE-16)/64.*DR)*CONDC(T(NFINE),T(NFINE-64),2)

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13W 0098
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13W 0153

NXT=RNGS-1
GO TO 200
120 NOX:(2)=NGES-NOXI(2)
  VP:=NGES-NOXI(2).GT.0) GO TO 130
  MEAN:=MPINE+NT:NOXI(2))/2
  NOXI(2)=(MEAN)/DOXID(2)*CONDUC(T(MPINE),T(MT:NOXI(2))),1)
  VARS=(VPIE-6+MT:NOXI(2))/2
  MSIP(2)=R(MEANS)/R(MPINE-64)-NOXI(2)
  1) *CONDUC(T(MPINE),T(MT:NOXI(2)))
  NVER:NGES)=NOXI(2)*MSIP(2)/NOXI(2)
  NVAPE=(MPINE-2+MT:NOXI(2))/2
  NCAP:NGES)=R(MEAN)*DOXID(2)*SPEC(TOXID(2),1)+R(MEANS)*
  1) *R(MPINE-32)-NOXI(2))*SPEC(TOXID(2),2)
NXT=RNGS-1
GO TO 200
130 NCAP:NGES)=6.0*DRAB(MPINE-4))*SPEC(T(MPINE),1)
  NT:(NOXI(2)=MPINE-NOXI(2)
  T:NT:NOXI(2))=TOXID(2)
  NOXI(2)=NOXI(2)+2
  NOXUP=NGES-1
  IP:(NOXI(2)=NGES) NVER:NGES)=R(MPINE-6)/16.0*4)
  1)CONDUC(T(MPINE),T(MPINE-16))
  IP:NOXUP.L.T.NOXI(2) GO TO 150
  NT:(NOXI(2)=MPINE-16
  MAX:=NT:NGES-1)
  DO 160 K=NOXI(2),NOXUP
  NT:(K)=MAX-16*(NOXUP-K)
  K:=K-1)
  NCAP(K)=16.0*DRAB(MT)*SPEC(T(MT),1)
  NVER(K)=R(MT-8)/16.0*DRAB)*CONDUC(T(MT),T(MT-16)),1)
  1)CONDUC(T(MT),T(MT-16))
  150 N1=NOXI(2)+1
  VP:(N1)=MPINE-NOXI(2)/16*16+16
  MEAN=(MT(M1)+MT:NOXI(2))/2
  NVER(M1)=R(MEAN)/DOXID(2)*CONDUC(T(MT(M1)),T(MT(M1))),1)
  1)CONDUC(T(MT(M1)),T(MT(M1)))
  NVAPE=(MT(M1)-16+MT:NOXI(2))/2
  NOXI(2)=R(MEAN)/DOXID(2)*R(MT(M1)-16))
  1)CONDUC(TOXID(2),T(MT(M1)-16)),1)
  N2=NOXI(2)-1
  NT:(N2)=MT:NOXI(2)-34)/64*64+1
  NVAPE=(MT(M2)+MT:NOXI(2))/2
  NVER(MOXI(2))=R(MEAN)/DOXID(2)*CONDUC(T(MT(M2)),T(MT(M2))),2)
  1)CONDUC(T(MT(M2)),T(MT(M2)))
  1)R(MT(M1)-8)
  P2=P:MT(M2)+32)
  NCAP(MOXI(2))=R(MEAN)*DOXID(2)*SPEC(TOXID(2),2)+
  1) (NOXI(2)+2-R1*2)*SPEC(TOXID(2),1))
NXT=RNGS-2
DO 250 K=NOXUP,MSIP
  N1:(K)=MT(MK-1)+64
  NVAPE(K)=R(MT(MK)-32)/64.0*DRAB)*CONDUC(T(MT(MK-1)),T(MT(MK))),2)
  NCAP(K)=68.0*DRAB(MT(K))*SPEC(T(MT(K)),2)
  250 CONTINUE
  IP(MSTART,EO,GO TO 2000
  DO 310 K=1,NGES
  310 QRFAC(K)=0.

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158 0154 QSUBP(1)=0.
159 0155 QSUBV(2)=0.
160 0156 IP(OPINED:1).GT.0.)QSUBP(1)=OPINED(1)*RSUBP(1)
161 0157 IP(OPINED:2).GT.0.)QSUBP(2)=OPINED(2)*RSUBV(2)
162 0158 IP(INDIPP(1).EQ.0.) GO TO 320
163 0159 OX=OXIGPL(1)*R(1)
164 0160 QSUBP(1)=QSUBP(1)-QSPILT*OXI
165 0161 QREACT(MOXI(1))=OXHEAT*OXI
166 0162 IP(MOXI(1).GT.1) GO TO 320
167 0163 QREACT(2)=NVER(2)*QREACT(1)/MOXI(1)
168 0164 QREACT(1)=QREACT(1)-NVER(2)/HEIR(1)
169 0165 320 IP(INDIPP(2).EQ.0.) GO TO 800
170 0166 OX=OXIGPL(2)*R(MPINE)
171 0167 QSUBP(2)=QSUBP(2)-QSPILT*OXI
172 0168 QREACT(MOXI(2))=OXHEAT*OXI
173 0169 IP(MOXI(2).NE.MGES) GO TO 800
174 0170 QREACT(MGRS-1)=NVER(MGES)*QREACT(MGES)/MOXI(2)
175 0171 QREACT(MGES)=QREACT(MGES)*NVER(MGES)/HEIR(2)
176 0172 800 CALL INTRN
177 0173 TOXID(1)=T(1)
178 0174 TOXID(2)=T(MPINE)
179 0175 IP(INDIPP(1).EQ.0.) GO TO 1200
180 0176 IP(MOXI(1).EQ.1) GO TO 1110
181 0177 M=MT(MOXI(1))
182 0178 M1=MT(MOXI(1))-1
183 0179 T(M1+16)=T(MC)-NVER(MOXI(1))*(T(M0)-T(M1))/MOXI(1)
184 0180 TOXID(1)=T(M0)
185 0181 GO TO 1200
186 0182 TOXID(1)=QREACT(1)/MOXI(1)+NVER(2)*(T(1)/HEIR(1)+T(65)/MOXI(1))
187 0183 T(17)=TOXID(1)
188 0184 1200 IP(INDIPP(2).EQ.0.) GO TO 2000
189 0185 IP(MOXI(2).EQ.MGES) GO TO 1210
190 0186 M=MT(MOXI(2))
191 0187 M1=MT(MOXI(2))-1
192 0188 T(M1+16)=T(M0)-NVER(MOXI(2))*(T(M0)-T(M1))/MOXI(2)
193 0189 TOXID(2)=T(M0)
194 0190 GO TO 2000
195 0191 1210 TOXID(2)=QREACT(MGES)/MOXI(2)+NVER(MGES)*
196 0192 (T(MPINE)/HEIR(2)+T(MPINE-64)/MOXI(2))
197 0193 T(MPINE-16)=TOXID(2)
198 0194 2000 IF(T(1).LT.2200.) RETURN
199 0195 WRITE(6,3000)
200 0196 3000 FORMAT(1RO,40TEMPERATURE HIGHER THAN 2200 DEG C
201 0197 CALL OUTPUT
202 0198 TIME=THAX
203 0199 RETURN
204 0200 END
205 0201
206 0202
207 0203
208 0204
209 0205
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211 0207
212 0208
213 0209
214 0210

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ISN 0002      SUBROUTINE TLUMB
C             TLUMB IS USED IF NLUMB=1 (UNIFORM TEMPERATURE) OR
C             NLUMB=2 (TEMPERATURE IS INPUT)
ISN 0003      IMPLICIT REAL*8 (A-H,O-Z)
ISN 0004      COMMON/GEOMET/ R (1000),ROXID (2),RALPA (2),WALL,DOXID (2),DALPA (2),DR
ISN 0005      COMMON/TEMP / T (1000),TOXID (2),TALPA (2),TSTART,TSTREAM (2),TWALL (2)
ISN 0006      COMMON/TEMPIN/ TCOOL (100,2),ETCOOL (100,2),TRAD (100,2),KTRAD (100,2)
ISN 0007      COMMON/HEAT / HVEA (100),HCOOL (2),FRADIA (2),HEATPL (2),OPIXED (2),
1             QSPLIT,HCAP (100),HSTEAM (2),HPADIA (2)
2             ,QSURF (2),QCOM (2),OPAD (2),ORFACT (2)
ISN 0008      COMMON/HEADLN/ NTITLE (20)
ISN 0009      COMMON/CONCEN/ C (1000),COXID (2),COXAL (2),CALBET (2),CGRPA (2),
1             OXIGPL (2),NDIFF (2),CSTAPT,GAIN (2)
2             ,OCAP (500),OVER (500),OUTMAX (500)
3             ,COA (2),CAO (2),CAB (2),CBA (2)
4             ,OCAPOA (2),OCAPO (2),OCAPOB (2),OCAPOA (2)
ISN 0010      COMMON/EXIT / TIME,TRAY,DTTEMP,DTDIFF,DTPRIN,DTMAX (100)
1             ,WTEMP,NDIFF,NDPRINT
ISN 0011      COMMON/MESH /NGROSS,NFINE,NOXID (2),NOXI (2)
1             ,NLUMB,NSTART,NALPA (2)
ISN 0012      COMMON/HEATHT/HT (100),HTCOOL (2),HTWALL (2),HTCOOL (2),HTWALL (2),NGEN
ISN 0013      COMMON/HTSICO/HC (500),HBAKER,NGEN,NOA (2),HAB (2)
1             ,NOA (2),HAA (2),HAB (2),HBA (2),INTOXI (2),INTB
2             ,NOA1,HAO1,HAB1,HBA1,NOXID1,NALPA1
3             ,NOA2,HAO2,HAB2,HBA2,NOXID2,NALPA2
ISN 0014      COMMON/HEATPRO/ DENZIN,DEWENO,OSTOCH,OXICOM,DEKRAI,PICFAC,OXHEAT
ISN 0015      COMMON/PROFIL/ CO (500),K (500),OLAYFR (2),ALAYER (2),BLAYER,COXID (2),
1             ,OALPA (2),OGAIN (2),OBTETA,OTOTAL,OBPTAS,STEMP,
2             ,M1,M2,M3,M4,M5,MURDER,NSCALF
ISN 0016      COMMON/INPUT/ NDIFFIN (100,2),TINDIP (100,2),HCOEFP (100,2),
1             TCOEFP (100,2),HRADCO (100,2),TRADCO (100,2),
2             QPLUXI (100,2),TOPLUX (100,2),TIMSTP (100),DTNEW (100),
3             NDIFFIN (2),NDIFFIN (2),KOPLUX (2),KOPLUX (2),
4             KCOEFP (2),KCOEFP (2),HRADCO (2),HRADCO (2),NSTEP
ISN 0017      IF (NLUMB.EQ.1) GO TO 1
ISN 0018      T (1) = TSTREAM (1)
ISN 0019      IF (TSTREAM (1).EQ.0.) T (1) = TSTREAM (2)
ISN 0020      GO TO 2000
ISN 0021      1 QREACT (1) = 0.
ISN 0022      IF (OPIXED (1).GT.0.) QREACT (1) = OPIXED (1) * R (1)
ISN 0023      IF (OPIXED (2).GT.0.) QREACT (1) = OPIXED (2) * R (NFINE) + QREACT (1)
ISN 0024      IF ((NDIFF (1) * NDIFF (2)).EQ.0.) GO TO 11
ISN 0025      NCAP (1) = .5 * R (1) ** 2 - ROXID (1) ** 2 + ROXID (2) ** 2 - R (NFINE) ** 2 *
ISN 0026      1 SPEC T (1, 1) + (ROXID (1) ** 2 - ROXID (2) ** 2) * SPEC T (1, 2)
ISN 0027      QREACT (1) = QREACT (1) + (OXHEAT - QSPLIT) * OXIGPL (1) * R (1) +
ISN 0028      1 OXIGPL (2) * R (NFINE)
ISN 0029      GO TO 13
ISN 0030      11 IF (NDIFF (1).EQ.0) GO TO 12
ISN 0031      NCAP (1) = .5 * R (1) ** 2 - ROXID (1) ** 2 * SPEC T (1, 1) +
ISN 0032      1 (ROXID (1) ** 2 - R (NFINE) ** 2) * SPEC T (1, 2)
ISN 0033      QREACT (1) = QREACT (1) + (OXHEAT - QSPLIT) * OXIGPL (1) * R (1)
ISN 0034      GO TO 13
ISN 0035      12 NCAP (1) = .5 * R (1) ** 2 - ROXID (2) ** 2 * SPEC T (1, 2) +
ISN 0036      1 (ROXID (2) ** 2 - R (NFINE) ** 2) * SPEC T (1, 1)
ISN 0037      QREACT (1) = QREACT (1) + (OXHEAT - QSPLIT) * OXIGPL (2) * R (NFINE)

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13 DTN=NCAP(1)/NVER(1)*NVER(2)
C*MAX(1)-DTN
NPAR=DTMP/DTN*1.
IP(DTN.GE.DTEMP) NPAR=1
NPAR=NPAR
DTN=DTMP/NPAR
IF(NSTART.EQ.0) GO TO 2000
DELTAQ=REACT(1)*HEATPL(1)*R(1) * HEATPL(2)*R(NPIMP)
DO 14 N=1, NPAR
14 T(1)=T(1)+DELTAQ*DTN/NCAP(1)
DO 15 I=1,2
QCON(I)=0.
IF(NCOOL(I).GT.0.) QCON(I)=NCOOL(I)*NSTRAN(I)-T(1)
QRAD(I)=0.
IF(HEATPL(I).GT.0.)
10RAD(I)=RADIA(I)*5.77E-12*(TSMALL(I)+273.16)**4 - (T(1)+273.16)**4)
HEATPL(I)=QCON(I)+QRAD(I)
15 CONTINUE
2000 T(NPIMP)=T(1)
TSUR(1)=T(1)
TSUR(2)=T(1)
TOXIS(1)=T(1)
TOXIS(2)=T(1)
RETURN
END

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15M 0002 SUBROUTINE INTTEMP
15M 0003 IN THIS SUBROUTINE THE TEMPERATURE INTEGRATION IS PERFORMED
15M 0004 IMPLICIT REAL*8 (A-N,O-S)
15M 0005 COMMON/GEOMRT/ T(1000),RHOID(3),RALPA(2),WALL,BOXID(2),DALPA(2),DR
15M 0006 COMMON/TEMP / T(1000),TOLID(2),TALPA(2),TSTRT,TSTEAM(2),TWALL(2)
15M 0007 1,STRT(2)
15M 0008 COMMON/THTTM/ TCOOL(100,2),STCOOL(100,2),TRAD(100,2),STRAD(100,2)
15M 0009 COMMON/HEAT / HVER(100),KCOOL(2),ERADIA(2),HEATFL(2),OPTIMP(2),
15M 0010 OPTIMP,HCAP(100),HSTEAM(2),HRADIA(2)
15M 0011 2,OSURP(2),OCOM(2),QRAD(2),QREACT(2)
15M 0012 COMMON/HEADLM/ HTTLB(20)
15M 0013 COMMON/CUSCRM/ C(1000),CORID(2),CORAL(2),CALBES(2),CBETA(2),
15M 0014 OXIDPL(2),HDTTP(2),CSTAR,DAIM(2)
15M 0015 2,OCAP(500),OYEM(500),ODTAX(400)
15M 0016 3,COR(2),CAO(2),CAB(2),CBA(2)
15M 0017 4,OCAPOA(2),OCAPAO(2),OCAPAB(2),OCAPBA(2)
15M 0018 COMMON/REIT / TIME,TMAX,DTTEMP,DTDTP,DTPRIM,TKMAX(100)
15M 0019 1,HTEMP,NDTTP,HRTIM
15M 0020 COMMON/RESM /MROSS,MPIRE,BOXID(2),MOXI(2)
15M 0021 1,MLURB,HSTART,MALPA(2)
15M 0022 COMMON/RESMIZ/MT(100),MTCOOL(2),MTWALL(2),MTCOOL(2),MTWALL(2),MREF
15M 0023 COMMON/RESMCO/MC(500),MBAKPP,MUF,MCA(2),MAB(2)
15M 0024 1,MOA(2),MAO(2),MAB(2),MBA(2),MBA(2),MBA(2),MTOXI(2),MTP
15M 0025 2,MOA1,MAO1,MAB1,MBA1,BOXID1,MALPA1
15M 0026 3,MOA2,MAO2,MAB2,MBA2,MCA1,MCA2,MAB2
15M 0027 COMMON/MATPRO/ DENSI,DEHMO,OSTOCH,OXICOH,DEMTRAT,PICPAC,ORHEAT
15M 0028 COMMON/PROFIL/ CO(500),E(500),OLATYP(2),ALAYER(2),BLAYER,ORHID(2),
15M 0029 1,MA1,M2,M3,M4,M5,NUMBER,NSCALE
15M 0030 COMMON/MINPOT/ MDTPTH(100,2),TMDTY(100,2),MCOEPP(100,2),
15M 0031 TCOEPT(100,2),HRADCO(100,2),BRADCO(100,2)
15M 0032 2,QLLXX(100,2),OPLUX(100,2),TIRSTP(100),DTM(100),
15M 0033 3,MIXIN(2),MIXIN(2),MOPLUX(2),MOPLUX(2),MOPLUX(2),
15M 0034 4,MCOEPP(2),MCOEPP(2),KRANCO(2),HRADCO(2),MSTEP
15M 0035 DIMENSION TR(1000)
15M 0036 TRM=DTTPP
15M 0037 DO 300 L=1,NBS
15M 0038 DTMAX(L)=HCAP(L)/(MVER(L)+MVER(L+1))
15M 0039 TP=DTMAX(L).LT.DTM) DTM=DTMAX(L)
15M 0040 L=EN-NBS-1
15M 0041 300 CONTINUE
15M 0042 DTMAX(L) IS THE MAXIMUM STABLE TIME STEP FOR EACH BODY
15M 0043 TP=DTM.NR.DTTEMP) GO TO 310
15M 0044 MMAX1
15M 0045 DO 400 400
15M 0046 MMAX=DTMPP/DTM+1.
15M 0047 MMAX=MMAX
15M 0048 DTM=DTTEMP/MMAX
15M 0049 DO 500 400 400
15M 0050 T=(MSTEAM(1)+HRADZA(1)).DT.O.) DO 600 610
15M 0051 TR(1)=T(1)+(MVER(2)+(M(17)))-T(1)) * OSURP(1)+ORFACT(1)) *
15M 0052 1,DTM/HCAP(1)
15M 0053 GO TO 450
15M 0054 610 TR(1)=T(1)+(MSTEAM(1)+(MSTEAM(1)-T(1))+HRADIA(1)+(MSTEAM(1)-T(1))
15M 0055 1,HWTR(2)+T(1)) * OSURP(1)+ORFACT(1)+DTM/HCAP(1)
15M 0056 650 T=(MSTEAM(2)+HRADZA(2)).DT.O.) GO TO 440

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138 0040      T(NPIME)=T(NPIME)+NVER(NDES)*T(NT(NDES-1))-T(NPIME)*QSURF(2)*
138 0041      QREACT(NDES)*DTH/MCAP(NDES)
138 0042      GO TO 500
138 0043      T(NPIME)=T(NPIME)+INSTAN(2)*TSTEAM(2)-T(NPIME)*HRADIA(2)*
138 0044      1(TALL(2)-T(NPIME))+NVER(NDES)*T(NT(NDES-1))-T(NPIME)
138 0045      2*QREACT(NDES)+QSORP(2)*DTH/MCAP(NDES)
138 0046      500 DO 550 N=2,LDES
138 0047      NTL=NT(N-1)
138 0048      NT=NT(N)
138 0049      NTP=NT(N+1)
138 0050      T(NTP)-T(NT)+NVER(N)*T(NTL)-T(NTP)+NVER(N+1)*T(NTP)-T(NTP)
138 0051      1*QREACT(N)+DTH/MCAP(N)
138 0052      550 CONTINUE
138 0053      DO 600 K=1,NDES
138 0054      600 T:NT(N)=C:N:NT(N)
138 0055      1000 CONTINUE
138 0056      TSURP(1)=T(1)
138 0057      TSURP(2)=T(NPIME)
138 0058      DO 1100 I=1,2
138 0059      QCON(I)=0.
138 0060      QRAD(I)=0.
138 0061      IP:NCOL(I)=GT.0.) QCON(I)=NCOL(I)*TSTEAM(I)-TSURP(I)
138 0062      IP:HRADIA(I)=GT.0.) QRAD(I)=HRADIA(I)*5.77E-12*
138 0063      1(TALL(I)+273.16)*24-(TSURP(I)+273.16)*24
138 0064      HRATPL(I)=QCON(I)+QRAD(I)
138 0065      1100 CONTINUE
138 0066      RETURN
138 0067      END

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ISN 0042      10 CONTINUE-
ISN 0043      40 CALL NBSMB
C             NBSMB DETERMINES MESH SIZE AND INTERPOLATES IF THERE IS A CHANGE
C             IN MESH SIZE
ISN 0044      NC(1)=1
ISN 0045      NBSZ=1
ISN 0046      IF(NDISP(1).EQ.0.) GO TO 100
ISN 0048      INT=INTOX(1)
ISN 0049      NL=1+INT
ISN 0050      XINT=XINT
ISN 0051      XDR=XINT*DP
ISN 0052      XDR2=XDR*.5
ISN 0053      OCAP(1)=(R(1)-0.25*XDR)*XDR2
ISN 0054      IP(NL,NB) 203,203,201
ISN 0055      201 DO 202 L=NL,NOA1,INT
ISN 0056      202 T(L)=T(1)
ISN 0057      GO TO 210
ISN 0058      203 IF(INT.EQ.16) GO TO 210
ISN 0060      IP(NOXI(1).GT.1) GO TO 205
ISN 0062      SLOPE=(T(1)-TOXID(1))/(R(1)-NOXID(1))
ISN 0063      DO 204 L=NL,NOA1,INT
ISN 0064      204 T(L)=T(L-INT)-XDR*SLOPE
ISN 0065      GO TO 210
ISN 0066      209 NN=NOXI(1)-1
ISN 0067      IC=1
ISN 0068      DO 207 N=1,NN
ISN 0069      SLOPE=(T(INT(N))-T(INT(N+1)))/(R(N)-R(N+1))
ISN 0070      DO 206 L=INT(N),16,INT
ISN 0071      TA=T(IC)
ISN 0072      IC=IC+L
ISN 0073      206 T(IC)=TA-XDR*SLOPE
ISN 0074      207 CONTINUE
ISN 0075      IP:(NOA1+INT).GE.NT(NN) GO TO 210
ISN 0077      NN1=NOA1-INT
ISN 0078      DO 208 L=IC,NN1,INT
ISN 0079      208 T(L)=T(L+INT)-XDR*SLOPE
ISN 0080      210 CONTINUE
ISN 0081      NA=1
ISN 0082      NN=NOA(1)
ISN 0083      DO 220 L=INT,NN,INT
ISN 0084      N=NA+INT
ISN 0085      NDIS=NDIS+1
ISN 0086      NC(NDIS)=N
ISN 0087      OCAP(NDIS)=R(N)*XDR
ISN 0088      ODFP(NDIS)=(R(N)-XDR2)/XDR*ODI*CON(T(N),O(NA),O(N),O(NA),1)
ISN 0089      NA=N
ISN 0090      220 CONTINUE
ISN 0091      OCAP(NDIS)=.9*OCAP(NDIS)
ISN 0092      NDFP=NDFP+1
ISN 0093      NA=NOA(1)
ISN 0094      NNRAN=.9*(R(NA)+NOXID(1))
ISN 0095      RDISP=R(NA)-NOXID(1)
ISN 0096      ODFP(NDIS)=NNRAN/RDISP*ODI*CON(T(N),O(NA),O(NA),O(NA),1)
ISN 0097      ODA(1)=NDIS
ISN 0098      NC(NDIS)=NOXID(1)
ISN 0099      ODISP(1)=NNRAN*ODISP
ISN 0100      NL=NA(1)
ISN 0101      NN=NA(1)

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154 0226 0D1P00(MBA2)-RALPA(2)
155 0227 0E0P(1)00PAM/0D1P0D1P00M(T(MBA2),T(ALPA(2),C(MBA2),CBA(2),1)
156 0228 0000)
157 0229 0AB(2)=1
158 0230 0C(1)=RALPA2
159 0231 0CAPM(2)=0PAM00D1P
160 0232 00 TO 510
161 0233 0D1P00(MALPA2-MALPA(1)/3
162 0234 0BA100ALPA10D1P
163 0235 0BA200ALPA2-0D1P
164 0236 0P(MLO00) 310,330,325
165 0237 0ALPA(2)=11
166 0238 0(MBA1)=11
167 0239 0(MBA2)=11
168 0240 00 TO 375
169 0241 02=(MALPA2-1)/0000001
170 0242 00=0L000
171 0243 0P(00,00,00,00) 00=0L-00
172 0244 0L000(T(0L)-T(MH))/0(MH)-P(MH)
173 0245 0ALPA(2)0T(MH)-0(MH)-RALPA(2)0SLOP
174 0246 0(MBA1)0T(MH)-(R(MH)-R(MBA1))00CP
175 0247 0(MBA2)0T(MH)-(R(MH)-R(MBA2))00L0P
176 0248 0(MBA1)=CBA(2)00,0
177 0249 0(MBA2)=C(MBA1)
178 0250 0M00MAB(1)01
179 0251 0C(MBA1)=MBA1
180 0252 0M000,00 0ALPA(1)0R(MBA1)
181 0253 0D1P00RALPA(1)-R(MBA1)
182 0254 0M00(M00)0M00M/0D1P0D1P00M(TALPA(1),T(MBA1),CBA(1),C(MBA1),1)
183 0255 0CAPM(1)0M00M0D1P
184 0256 0CAP(MAB(1))0CAPM(1)0CAPM(1)
185 0257 0M000,00 0(MBA1)0R(MBA2)
186 0258 0D1P00R(MBA1)-R(MBA2)
187 0259 0CAP(M0P)00,00M00M0D1P
188 0260 0M00M0001
189 0261 0C(MBA1)=MBA2
190 0262 0M0P(M00)0M00M/0D1P0D1P00M(T(MBA1),T(MBA2),C(MBA1),C(MBA2),1)
191 0263 0C1P(1,01)0CAP(M00-1)
192 0264 0M00M0001
193 0265 0C(0000)0ALPA2
194 0266 0AB(2)=000
195 0267 0M000,00 0(MBA2)0RALPA(2)
196 0268 0D1P00R(MBA2)-RALPA(2)
197 0269 0M00(M00)0M00M/0D1P0D1P00M(T(MBA2),T(ALPA(2),C(MBA2),CBA(2),1)
198 0270 0CAPM(2)=0PAM00D1P
199 0271 00 TO 510
200 0272 0P(M0D1P(1),0T,0,0) 00 TO 340
201 0273 0M00M00
202 0274 0M00M000
203 0275 0M02=0000
204 0276 0M0P(1)00
205 0277 0M00MBA2-00M0P
206 0278 0M00M00,00 00 TO 105
207 0279 0CAP(1)0P(1)00,00
208 0280 0L01
209 0281 00 TO 100
210 0282 0CAP(1)00
211 0283 0(MBA2,1,1,000001) M00M00M00

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120 0021 000 BA=HMA
120 0022 BL=HMA,INTP
120 0023 DO 400 L=1,MM,INTP
120 0024 HMA=HMA+1
120 0025 MC(HMA)=L
120 0026 OVR(HMA)=R(L)-HMA/HORRIPCON(T(HA),T(L),C(HA),C(L),T)
120 0027 OCAP(HMA)=C(L)*OVR
120 0028 HA=L
120 0029 CONTINUE
120 0030 OCA=(HMA+OVR)/OCAP(HMA)
120 0031 TP(HORRIP(2),NO,0.) GO TO 1000
120 0032 TALPA(2)=T(L)
120 0033 HMA=HMA+50*(HMA2)/HALPA(2)
120 0034 HPTP=HMA2-HALPA(2)
120 0035 TP(L)=HMA2-OVR TALPA(2)=T(HMA2)-SLOP*HPTP
120 0036 HMA=HMA+1
120 0037 HAD(2)=HMA2
120 0038 MC(HMA2)=HALPA2
120 0039 OVR(HMA2)=HMA2/HORRIPCON(T(HMA2),TALPA(2),C(HMA2),C(L),T)
120 0040 OCAP(HMA2)=OCAP*HPTP
120 0041 INT=INT+OVR(2)
120 0042 INT=INT
120 0043 HMA=HMA+INT
120 0044 HPTP=HPTP
120 0045 TP(L)=HMA2
120 0046 TP(L)=HMA2
120 0047 DO 512 L=HMA2,MM,INT
120 0048 T(L)=T(L)
120 0049 GO TO 100
120 0050 HA=HMA2-1/600000
120 0051 BL=HA+0
120 0052 TP(L)=HORRIP(2)*515,515,520
120 0053 SLOP=T(HA)-T(L)/R(HA)-R(L)
120 0054 GO TO 512
120 0055 SLOP=T(HA)-TORRIP(2)/R(HA)-TORRIP(2)
120 0056 T(HMA2)=TALPA(2)-SLOP*(HALPA(2)-R(HMA2))
120 0057 HMA=HMA+1
120 0058 MC(HMA2)=HMA2
120 0059 HMA=HMA+50*(HALPA(2))/HMA2
120 0060 HPTP=HALPA(2)-R(HMA2)
120 0061 OVR(HMA2)=HMA2/HORRIPCON(TALPA(2),T(HMA2),C(HMA2),C(L),T)
120 0062 OCAP(HMA2)=OCAP*HPTP
120 0063 OCAP(HMA2)=OCAP*HPTP
120 0064 HMA=HMA+1
120 0065 TP(L)=HMA2
120 0066 TP(L)=HMA2,MM,INT
120 0067 DO 536 L=HMA2,MM,INT
120 0068 T(L)=T(L)
120 0069 GO TO 600
120 0070 HMA=HMA+1
120 0071 BL=HA+0
120 0072 TP(L)=HORRIP(2)*505,505,550
120 0073 SLOP=T(HA)-T(L)/R(HA)-R(L)
120 0074 GO TO 555
120 0075 SLOP=T(HA)-TORRIP(2)/R(HA)-TORRIP(2)
120 0076 HMA=HMA+1
120 0077 TP(L)=HMA2,MM,INT
120 0078 DO 560 L=HMA2,MM,INT
120 0079 T(L)=T(L)
120 0080 SLOP=HPTP

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130 0442 IP:MM,SO,MAOZ) GO TO 600
131 0443 MAWA=08
132 0444 MATH=NOINT
133 0445 GO TO 500
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ISM 0545      1000 IP (PALPA(1) - PALPA(2)) - LT - 4 - *DR) GO TO 6000
ISM 0546      IP:NDIPP(1) - 0 - 0 - GO TO 1310
ISM 0547      STOROA(1) = .5 * (C(MO1) + COA(1)) * OCAPOA(1) +
ISM 0550      .5 * (C(MA1) + CAO(1)) * OCAPAO(1) +
ISM 0551      .5 * (C(MB1) + CAB(1)) * OCAPAB(1) +
ISM 0552      .5 * (C(MB1) + CAB(1)) * OCAPBA(1)
ISM 0553      STOROA(2) = STOROA(1) + OVER(MOA(2)) * C(MO2)
ISM 0554      - OVER(MOA(1)) + CAO(1) - C(MA1)
ISM 0555      STORAB(1) = STORAB(1) + OVER(MAB(1)) * C(MB1)
ISM 0556      - OVER(MAB(1)) + C(MB1) - C(MB1)
ISM 0557      C(MC(MO1(1))) = COA(1)
ISM 0558      C(MC(MAB(1))) = CBA(1)
ISM 0559      1310 IP:NDIPP(2) - 0 - 0 - GO TO 1315
ISM 0560      STOROA(2) = .5 * (C(MO2) + COA(2)) * C(MO2) +
ISM 0561      .5 * (C(MA2) + CAO(2)) * C(MA2) +
ISM 0562      .5 * (C(MB2) + CAB(2)) * C(MB2) +
ISM 0563      .5 * (C(MB2) + CAB(2)) * C(MB2)
ISM 0564      STOROA(2) = STOROA(2) + OVER(MOA(2)) * C(MO2)
ISM 0565      - OVER(MOA(1)) + CAO(1) - C(MA1)
ISM 0566      STORAB(2) = STORAB(2) + OVER(MAB(2)) * C(MB2)
ISM 0567      - OVER(MAB(1)) + C(MB1) - C(MB1)
ISM 0568      C(MC(MO2(1))) = COA(2)
ISM 0569      C(MC(MAB(2))) = CBA(2)
ISM 0570      1315 IP:INSTANT, NR, 1) GO TO 5000
ISM 0571      CALL INTDIP
ISM 0572      IN THIS SUBROUTINE THE CONCENTRATION INTEGRATION IS PERFORMED
ISM 0573      IP:NDIPP(1) - 0 - 0 - GO TO 2100
ISM 0574      CALL INTFAC(TOXID(1), COA(1), CAO(1), 1)
ISM 0575      OCAPAO(1) = OCAP(MO1(1)) * C(MO1) + COA(1) - 2 * STOROA(1) /
ISM 0576      1 * (MO1) + COA(1) - C(MA1)
ISM 0577      OCAPBA(1) = OCAP(MB1(1)) * C(MB1) + CAB(1) - 2 * STORAB(1) /
ISM 0578      1 * (MB1) + CAB(1) - C(MB1)
ISM 0579      IP(OCAPBA(1) - 0.5 * OCAP(MB(1))) - LT - OCAP(MB(1)) GO TO 1400
ISM 0580      CALL OUTPBT
ISM 0581      OCAPBA(1) = 0.5 * OCAP(MB(1))
ISM 0582      WRITE(6, 1399)
ISM 0583      1399 FORMAT(1X, 30ALPHA/BETA INTERSPACE FIXED)
ISM 0584      1400 OCAPAB(1) = OCAP(MAB(1)) - OCAPBA(1)
ISM 0585      TOXID(1) = R(MA1) + 2 * OCAPAO(1) / (MO1D(1) + R(MA1))
ISM 0586      PALPA(1) = R(MB1) + 2 * OCAPBA(1) / (MB1D(1) + R(MB1))
ISM 0587      PALPA(1) = R(1) - PALPA(1)
ISM 0588      GAIN(1) = GAIN(1) * OXIGPL(1) * OXDIF
ISM 0589      OXIGPL(1) = OVER(2) * (C(1) - C(MC(2))) / R(1)
ISM 0590      IP:OXIGPL(1) - 1E-0.1 OXIGPL(1) - NDIPP(1)
ISM 0591      2100 IP:NDIPP(2) - 0 - 0 - GO TO 2500
ISM 0592      CALL INTFAC(TOXID(2), COA(2), CAO(2), 1)
ISM 0593      OCAPAO(2) = OCAP(MO2(1)) * C(MO2) + COA(2) - 2 * STOROA(2) /
ISM 0594      1 * (MO2) + COA(2) - C(MA2)
ISM 0595      OCAPBA(2) = OCAP(MB2(1)) * C(MB2) + CAB(2) - 2 * STORAB(2) /
ISM 0596      1 * (MB2) + CAB(2) - C(MB2)
ISM 0597      IP(OCAPBA(2) - 0.5 * OCAP(MB(2))) - LT - OCAP(MB(2)) GO TO 2400
ISM 0598      OCAPBA(2) = 0.5 * OCAP(MB(2))
ISM 0599      WRITE(6, 1399)

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ISM 0599
ISM 0600
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ISM 0616

2500 OCAPAB(2)=OCAP(HAB(2))-OCAPBA(2)
    ROZD(2)=R(MO2)-2.*OCAPAC(2)/ROZID(2)+R(MAO2)
    HALPA(2)=R(HA2)-2.*OCAPPA(2)/HALPA(2)+R(MBA2)
    DOZID(2)=ROZID(2)-R(MVIME)
    DALPA(2)=HALPA(2)-R(MVIME)
    GAIN(2)=GAIN(2)+ORIGPL(2)+DODIPP
    ORIGPL(2)=OVRT(MGES)+C(MVIME)-C(MC;MGIS-1))/R(MVIME)
    IFOXIGPL(2)=L.E.O.) ORIGPL(2)+HDI PP(2)
2500 CONTINUE
5000 RTTART=1
    RETURN
6000 WRITE(6,6001)
6001 POPRAT(1MO,40NBETA-ZINCALOY LESS THAN .005 CM THICK )
    CALL OUPUT
    TIME=TIME+TMAX
    RETURN
END

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ISN 0002      SUBROUTINE DSTART
C             DSTART PERFORMS THE CONCENTRATION CALCULATION IF OXIDE OR ALPHA
C             LAYER ARE THIN
ISN 0003      IMPLICIT REAL*8 (A-N,O-Z)
ISN 0004      COMMON/GEOMET/ R(1000),ROXID(2),HALFA(2),WALL,DOXID(2),DALFA(2),DR
ISN 0005      COMMON/TEMP / T(1000),TOXID(2),ALPHA(2),TSTART,TSTEAM(2),TWALL(2)
1,TSURF(2)
ISN 0006      COMMON/TEMPIN/ TCOOL(100,2),STCOOL(100,2),TRAD(100,2),STRAD(100,2)
ISN 0007      COMMON/HEAT / HVEN(100),HCOOL(2),HRADIA(2),HEATPL(2),QFIXED(2),
1          QSPLIT,HCAP(100),HSTEAM(2),HRADIA(2)
2          QSURF(2),QCON(2),QRAD(2),QREACT(2)
ISN 0008      COMMON/HEADLN/ WTITLE(20)
ISN 0009      COMMON/CONCEN/ C(1000),COXID(2),COXAL(2),CALBET(2),CBETA(2),
1          OXISPL(2),NDIFF(2),CSTART,GAIN(2)
2          OCAP(500),OVER(500),OBTMAX(500)
3          COA(2),CAO(2),CAB(2),CBA(2)
4          OCAPOA(2),OCAPAO(2),OCAPAB(2),OCAPBA(2)
ISN 0010      COMMON/ZEIT / TIME,TMAX,DTTEMP,DTDIFF,DTPRIN,DTMAX(100)
1,          NTEMP,NDIFF,NPRINT
ISN 0011      COMMON/RESN /NGROSS,NFINE,NOXID(2),NOXI(2)
1,          NLWNS,NSTART,NALPA(2)
ISN 0012      COMMON/RESNTE/NT(100),NTCOOL(2),NTWALL(2),NTCOOL(2),NTWALL(2),NGES
ISN 0013      COMMON/RESNCO/NC(500),NBAKER,NGES,NOA(2),NAB(2)
1,          NOA(2),NAO(2),NAB(2),NBA(2),INTOXI(2),INTN
2,          NOA1,NAO1,NAB1,NBA1,NOXI01,NALPA1
3,          NOA2,NAO2,NAB2,NBA2,NOXI02,NALPA2
ISN 0014      COMMON/MATPRO/ DENSI,DEWENO,OSTOCH,OXICOM,DEHRA,PTCPAC,ORHEAT
ISN 0015      COMMON/PROFIL/ CO(500),X(500),OLAYER(2),ALAYER(2),BLAYER,OOXID(2),
1          IOALFA(2),OGAIN(2),CBETA,OTOTAL,OBETA,STEMP,
2          ZH1,Z2,Z3,Z4,Z5,NUMBER,NSCALE
ISN 0016      COMMON/MINPUT/ NDIFIN(100,2),TINDIF(100,2),HCOEFF(100,2),
1          TCOEFF(100,2),NRADCO(100,2),TRADCO(100,2),
2          QPLUXI(100,2),TOPLUX(100,2),TINSTE(100),DTHEW(100),
3          NDIFIN(2),NDIFIN(2),NOPLUX(2),NOPLUX(2),
4          HCOEFF(2),HCOEFF(2),NRADCO(2),NRADCO(2),NSTEP
ISN 0017      DIMENSION CH(1000),STOXA(2),STORAB(2)
1          DALOLD(2),ALPAFL(2),BETAFL(2),COXOLD(2),CALOLD(2),CBOLD(2)
IF(NSTART.NE.2) GO TO 5500
1 NGES=NGROSS
DO 21 K=1,2
IF(NDIFF(K).EQ.0.) GO TO 21
QSURF=C(1)
IF(K.EQ.2) OSURF=C(NFINE)
CBET=C(NF1)
IF(K.EQ.2) CBET=C(NF2)
COXOLD(K)=0.5*(QSURF+COA(K))
CBOLD(K)=0.5*(CBET+CBA(K))
CALOLD(K)=0.5*(CAO(K)+CAB(K))
DALOLD(K)=DALFA(K)-DOXID(K)
ISN 0034      CALL INTFAC(TOXID(K),COA(K),CAO(K),1)
ISN 0035      CALL INTFAC(TOXID(K),CAB(K),CBA(K),2)
ISN 0036      IF(COXOLD(K).LT.COA(K)) COXOLD(K)=0.5*(COA(K)+OXICOM)
ISN 0038      IF(CALOLD(K).LT.CAB(K)) CALOLD(K)=0.5*(CAB(K)+CAO(K))
ISN 0040      IF(K.EQ.2) GO TO 2
ISN 0042      T1=T(1)
ISN 0043      C(1)=OXICOM

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ISM 0113 IP(CALPA(K)-DIXID(H)).GT.1.00001D-7) GO TO 430
ISM 0114 IP(R-1) EQ 010,020
ISM 0115 CBAN1 =ALPAPL(1)*NDIP1/DIPBT*C(MP1)
ISM 0116 IP(CBAN1.GT.CBA(1)) GO TO 415
ISM 0117 CBA(1)=CBAN1
ISM 0118 MP1=ALPAPL(1)
ISM 0119 CBOLD(1)=CBOLD(1)*CBA(1)-CALOLD(1)
ISM 0120 CAB(1)=CBA(1)
ISM 0121 CAO(1)=CAO(1)
ISM 0122 CALOLD(1)=CALOLD(1)
ISM 0123 GO TO 430
ISM 0124 CBAN2 =ALPAPL(2)*NDIP2/DIPBT*C(MP2)
ISM 0125 IP(CBAN2.GT.CBA(2)) GO TO 425
ISM 0126 CBA(2)=CBAN2
ISM 0127 MP2=ALPAPL(2)
ISM 0128 CBOLD(2)=CBOLD(2)*CBA(2)-CALOLD(2)
ISM 0129 CAB(2)=CBA(2)
ISM 0130 CAO(2)=CAO(2)
ISM 0131 CALOLD(2)=CALOLD(2)
ISM 0132 IP(DIXID(K).GT.1.0-7) GO TO 490
ISM 0133 IP(R-1) EQ 040,050
ISM 0134 COA(1)=COA(1)*PICFAC
ISM 0135 C(1)=COA(1)
ISM 0136 COXOLD(1)=COA(1)
ISM 0137 GO TO 490
ISM 0138 COA(2)=COA(2)*PICFAC
ISM 0139 C(MP1)*COA(2)
ISM 0140 COXOLD(2)=COA(2)
ISM 0141 IP:(K.EQ.1).AND.(NDIPP(2).GT.0.1) GO TO 21
ISM 0142 N1=ND-2
ISM 0143 N1=ND-2
ISM 0144 DO 20 N=1,MAX
ISM 0145 DO 16 L=ND,NO,2
ISM 0146 CH(L)=C(L)*FACTOR*(C(L+2)+C(L-2))-2.*C(L)
ISM 0147 IP(NDIPP(1).EQ.0.) GO TO 17
ISM 0148 IP(CBA(1).NE.CBAN1)
ISM 0149 BETA(1)=BETAPL(1)*BPL1
ISM 0150 CH(MP1)=C(MP1)*BPL1*DIPBT*(C(MP1)-C(MP1))/DELTA*DTM
ISM 0151 /(.9*NDIP1+.75*DM)
ISM 0152 CH(MP1)=C(MP1)*(C(MP1+2)+C(MP1-2))-2.*C(MP1)*DTM*DIPBT
ISM 0153 /(.125*DELTA*DM)
ISM 0154 C(MP1)*DM = C(MP1)*2.*FACTOR
ISM 0155 IP(NDIPP(2).EQ.0.) CH(MP1)=C(MP1)/NDIP2
ISM 0156 IP(R.EQ.1) GO TO 18
ISM 0157 IP(CBA(2).NE.CBAN2)
ISM 0158 BETA(2)=BETAPL(2)*BPL2
ISM 0159 CH(MP2)=C(MP2)*BPL2*DIPBT*(C(MP2)-C(MP2))/DELTA*DTM
ISM 0160 /(.9*NDIP2+.75*DM)
ISM 0161 CH(MP2)=C(MP2)*(C(MP2+2)+C(MP2-2))-2.*C(MP2)*DTM*DIPBT
ISM 0162 /(.125*DELTA*DM)
ISM 0163 IP(NDIPP(1).EQ.0.) CH(1)=C(1)+2.*FACTOR*(C(2)-C(1))
ISM 0164 DO 19 L=MP1,MP2
ISM 0165 C(L)=CH(L)
ISM 0166 CONTINUE
ISM 0167 IP(NDIPP(1).GT.0.) BETAPL(1)=BETAPL(1)/MAX
ISM 0168 IP(NDIPP(2).GT.0.) BETAPL(2)=BETAPL(2)/MAX

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21 CONTINUE
DO 35 K=1,2
  IF (NDLPP(K).EQ.0.) GO TO 35
  DSTOR = DOXIDP(LN) - DALPA(LN) * DTDIPP
  OSURP = C(1)
  IF (K.EQ.2) OSURP = C(NPINE)
  CREAM = 0.5 * OSURP * COA(K)
  DOXID(K) = DOXID(K) + DSTOR * DOXID(K) * (COOLD(K) - CREAM)
  / (CREAM - CA * OLD(K))
  IF (DOXID(K) .LT. 1.00E-7) DOXID(K) = 1.E-7
  NOXID = DOXID(K) / DR
  DOXID(K) = DOXID(K) / DR * .5
  DSTOR = ALPA(LN) - BETAP(LN) * DTDIPP
  CREAM = 0.5 * COA(K) * CAB(K)
  DALPA(K) = DALPA(K) + DSTOR * DALOLD(K) * (CALOLD(K) - CREAM)
  / (CREAM - CBOLD(K))
  IF (DALPA(K) .LT. (DOXID(K) * 1.00E-7)) DALPA(K) = DOXID(K) * 1.E-7
  WALPA = DALPA(K) / DR
  DALPA(K) = DALPA(K) / DR * .5
  IF (K.EQ.2) GO TO 25
  DOXID(1) = R(1) - DOXID(1)
  DALPA(1) = R(1) - DALPA(1)
  NGES = NGES + 1
  NOA(1) = 2
  NC(2) = NOXID(1) * 1
  NAB(1) = 3
  NC(3) = WALPA(1) * 1
  IF (DOXID(1) .LT. 6.E-8) .OR. (DALPA(1) - DOXID(1) .LT. 6.E-8)) GO TO 30
  NL = 2
  NN = NOXID * 1
  CDIPP = C(1) - COA(1) / DOXID(1) * DR
  DO 22 L=NL, NR
  C(1) = C(1) - CDIPP
  NL = NL + 1
  SLOPE = CAO(1) - CAB(1) / (DALPA(1) - DOXID(1))
  C(NL) = CAO(1) - SLOPE * (DOXID(1) - R(NL))
  NL = NL + 1
  IF (NL .LE. NALPM + 1) GO TO 24
  GO TO 30
25 DOXID(2) = R(NPINE) * DOXID(2)
  DALPA(2) = R(NPINE) * DALPA(2)
  NGES = NGES + 1
  NOA(2) = NGES - 1
  NC(MOA(2)) = NPINE * NOXID(2)
  NAB(2) = NGES - 2
  NC(NAB(2)) = NPINE * WALPA(2)
  IF (DOXID(2) .LT. 6.E-8) .OR. (DALPA(2) - DOXID(2) .LT. 6.E-8)) GO TO 30
  NN = NPINE * 1
  SLOPE = C(NPINE) - COA(2) / DOXID(2)
  C(NL) = C(NPINE) - SLOPE * (NL - R(NPINE))
  CDIPP = SLOPE * DR
  NL = NL + 1
  DO 26 L=NL, NR
  C(1) = C(1) - CDIPP
  NN = NN + 2
  NL = NPINE * 2
  SLOPE = CAO(2) - CAB(2) / (DALPA(2) - DOXID(2))

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15H 0201 C(M)=CAO(2)-I*(M)-ROXD(2)*SLOPE
15H 0202 C(M)=CAO(2)-(M(M)-ROXD(2))*SLOPE
15H 0203 M=M-1
15H 0204 M=NL+1
15H 0205 CDIPP=SLOP*DP
15H 0206 DO 27 I=M,N
15H 0207 C(I)=C(I-1)+CDIPP
15H 0208 30 DATA(M)=DATA(M)+XIGPL(M)*D*DIPP
15H 0209 34 CONTINUE
15H 0210 MC(MDS)=MDS
15H 0211 MAXMERS=12
15H 0212 I=(MDS)/I*.GT.0.) GO TO 37
15H 0213 DO 16 M=2,MAX
15H 0214 MC(M)=M*(M-1)*60
15H 0215 I=(MC(M).GT.MP2-10) MC(M)=MC(M-1)
15H 0216 I=(MLOMB.GT.0) I*(MC(M))=I(I)
15H 0217 36 CONTINUE
15H 0218 GO TO 45
15H 0219 37 HALPH=DALPA(1)/DB
15H 0220 MPM=(HALPH+1)/2+3
15H 0221 I=(MPM-MP1) 237,337,137
15H 0222 137 M=MP1+2
15H 0223 SLOPE=MC(MP1)-C(M1)/(R(MP1)-R(M1))
15H 0224 C(MP)=C(MP1)-I*(MP1)-M*(MPM)*SLOPE
15H 0225 M1=M+1
15H 0226 GO TO 337
15H 0227 237 SLOPE=(CBA(1)-C(MP1))/I*(ALFA(1)-R(MP1))
15H 0228 C(MP)=C(MP1)+R(MP1)-I*(MP1)*SLOPE
15H 0229 M1=M+1
15H 0230 DO 38 M=5,12
15H 0231 MC(M)=MC(M-1)+2
15H 0232 I=(MC(M).GT.MP2) MC(M)=MP2
15H 0233 38 CONTINUE
15H 0234 MC(13)=MC(12)+63/60*60+1
15H 0235 I=(MDS/2) 130,130,130
15H 0236 130 HALPH=2.42,40
15H 0237 MPO=MP1
15H 0238 GO TO 140
15H 0239 MPO=MP2-10
15H 0240 DO 39 M=14,MAX
15H 0241 MC(M)=MC(M-1)+60
15H 0242 I=(MC(M).GT.MPO) MC(M)=MC(M-1)
15H 0243 39 CONTINUE
15H 0244 I=(MLOMB)*2.42,40
15H 0245 40 DO 41 M=2,MAX
15H 0246 41 I*(MC(M))=I(I)
15H 0247 -ALFA(1)=I(1)
15H 0248 GO TO 44
15H 0249 42 SLOPE=(ROXD(1)-I*(65))/I*(ROXD(1)-I*(65))
15H 0250 TALPA(1)=ROXD(1)-SLOPE*(ROXD(1)-TALPA(1))
15H 0251 DO 43 M=6,12
15H 0252 I*(MC(M))=SLOPE*(ROXD(1)-TALPA(1))
15H 0253 43 I*(MDS/2).EQ.0.) GO TO 5000
15H 0254 44 HALPH=DALPA(1)/DB
15H 0255 MPM=MP1+1
15H 0256 I=(MP2-MPM) 245,305,145
15H 0257 45 M=MP2-2
15H 0258 145 M=MP2-2

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203 0.370

SLOPE=(C(NP2)-C(MH))/R(MH)-R(NP2)
C(NP2)=C(NP2)-(R(NP2)-R(NP2))*SLOPE
NP2=NP
GO TO 345
245 SLOPE=(CBA(2)-C(NP2))/(R(NP2)-R(ALPA(2)))
C(NP2)=C(NP2)+(R(NP2)-R(NP2))*SLOPE
NP2=NP
345 KC(MOES-3)=NP2
KC(MOES-11)=KC(MOES-3)-16
NL=MOES-10
NR=MOES-8
DO 47 N=NL,NH
KC(N)=KC(N-1)+2
XP(KC(N-1),LT,MP) KC(N-1)=NP*
47 CONTINUE
XP(KC(MOES-11),LT,MP) KC(MOES-12)=KC(MOES-11)-2
NL=MOES-11
NR=MOES-3
XP(NL,NH),53,53,51
51 DO 52 N=NL,NH
52 T(KC(N))=T(1)
TALPA(2)=T(1)
GO TO 5000
53 NP=NP*ME-66
SLOPE=(T(NP)-TOXID(2))/R(NP) )-NOXID(2)
DO 49 N=NL,NH
T(KC(N))=T(NP)-SLOPE*(R(NP)-R(KC(N)))
TALPA(2)=T(NP)-SLOPE*(R(NP)-R(ALPA(2)))
5000 RETURN
5500 XP(TXNB,NO,0.) GO TO 6000
NL=1
NR=MOES
XP(NDIPP(1),GT,0.) NL=NR+1(1)+10
XP(NDIPP(2),GT,0.) NR=NR+2(1)-10
5600 NL=KC(NL)
NR=KC(NL+1)
CDIPP=2.0*NR(KC(NL)-C(NH))/R(NL)-R(NH)
NL=NL+2
NR=NR-2
XP(NL,GT,NR) GO TO 5600
DO 5700 N=NL,NH,2
5700 C(N)=C(N-2)-CDIPP
5800 NL=NL+1
XP(NL,LT,NR) GO TO 5600
NOXID(1)=NOXID(1)/DR
NOXID(2)=NOXID(2)/DR
TALPA(1)=TALPA(1)/DR
TALPA(2)=TALPA(2)/DR
NR=NR+NOXID
NL=2
KC(1)=1
DO 6100 L=1,MP*NB,2
6100 CH(L)=C(L)
XP(NDIPP(1),NO,0.) GO TO 6500
NR=NR+NOES+1
NO(1)=2
NR(1)=1
KC(2)=1+NOXID(1)

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130 0371
130 0372
130 0373
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130 0375
130 0376
130 0377
130 0378
130 0379
130 0380
130 0381
130 0382
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130 0384
130 0385
130 0386
130 0387
130 0388
130 0389
130 0390
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130 0395
130 0396
130 0397
130 0398
130 0399
130 0400
130 0401
130 0402
130 0403
130 0404
130 0405

NC (1) = 10 NALPA (1)
NALP = NALPA (1) / DP
NC (2) = (NALP (1) / 2) * 3
NP1 = NC (2)
NC (1) = 205
NO 6000 N=5, 12
NC (1) = NC (1) - 1) * 2
RLD=10
QMR=0000
IP (0000) (1) . 00 . 0 . 1 GO TO 7150
0000 0000 0000 11
NOA (2) = 0000-1
NAB (2) = 0000-2
NC (0000) = 0000
NC (NOA (2)) = NP1 NB = NO 120 (2)
NC (NAB (2)) = NP2 NB = NALPA (2)
NALPB = NALPA (2) / 00
NC (NAB (2) - 3) = NP2 NB = (NALP (1) / 2) * 2 - 3
0000
NP2 = NC (1) (0000 - 3)
NL = 0000 - 10
NC (NL - 3) = NC (NAB (2) - 3) - 16
NP = 0000 - 6
NAB = 0000 - 12
NO 7100 N=0, 00
NC (1) = NC (1) - 1) * 2
7150 NO 7200 N=0, 00
7200 NC (1) = NC (1) - 1) * 04
IP (0000) (1) . 00 . 3 GO TO 1
CALL 0000
TNR=0000
BTR=0000
0000


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I 0002 SUBROUTINE RESUME
I 0003 RESUME DEFINES MESH SIZE AND INTERPOLATES IF THERE IS A CHANGE
I 0004 IN MESH SIZE
I 0005 IMPLICIT REAL*8 (A-H,O-S)
I 0006 COMMON/MSHNT/ N(1000),NOXID(2),HALPA(2),WALL,NOXID(2),DALPA(2),DR
I 0007 COMMON/TEMP / T(1000),TOXID(2),HALPA(2),START,STOPAN(2),TWALL(2),
1,TEMP(2)
I 0008 COMMON/THIN/ TCOOL(100,2),STCOOL(100,2),TPAD(100,2),STRAN(100,2)
I 0009 COMMON/HEAT / HVER(100),MCOOL(2),ERABH(2),HEATP(2),OPENED(2),
1,OSPLIT,MCAP(100),MSTRAN(2),MPADIA(2)
I 0010 2,OSBPP(2),OCN(2),ORAD(2),ORACT(2)
I 0011 COMMON/HEARL/ RTTL(20)
I 0012 COMMON/CONCR/ C(1000),CORID(2),CONFL(2),CALRET(2),CBETA(2),
I 0013 OXID(2),NDIPP(2),NDIPP(2),CSTART,DATA(2)
I 0014 3,OCAP(500),OVER(500),OSTWAX(500)
I 0015 COA(2),CAO(2),CAB(2),CBA(2)
I 0016 COMMON/OCAP(2),OCAPAO(2),OCAPAB(2),OCAPBA(2)
I 0017 COMMON/REIT / TIME,TMAX,DTSTEP,DTDIR,DTDIRN,DTMAX(100)
1,STEP,NDIPP,NDIPPIN
I 0018 COMMON/RESH /MROSS,RTIME,NOXID(2),NOX(2)
I 0019 COMMON/MSHNT/NT(100),MTCOOL(2),MFWALL(2),MCOOL(2),MFWALL(2),MSPR
I 0020 COMMON/MSMCO/MC(500),MBAKER,MDS,MOA(2),MAB(2)
1,MOA(2),MBO(2),MAB(2),MBA(2),MTOXI(2),MTR
2,MOA1,MOA2,MOA3,MOA4,MOA5,MOA6,MOA7,MOA8,MOA9,MOA10,MOA11,MOA12
3,MOA13,MOA14,MOA15,MOA16,MOA17,MOA18,MOA19,MOA20,MOA21,MOA22,MOA23
I 0021 COMMON/MATPRO/ DBEIN,DESMO,OSTOCM,CHTCM,DMBAT,PICFAC,OKHEAT
I 0022 JALPA(2),OBLIN(2),OBLTA,OTOTAL,OBETA,S,TEMP,
1,M1,M2,M3,M4,M5,MWBEB,MSCALE
I 0023 COMMON/MINPT/ MBLP(100,2),TIMDIP(100,2),MCOBPP(100,2),
I 0024 TCOBPP(100,2),MBAICO(100,2),TRADCO(100,2),
I 0025 OPLIN(100,2),TOPLIN(100,2),FIRSTP(100),DTIME(100),
I 0026 NDIPPIN(2),NDIPPIN(2),NOPLIN(2),NOPLIN(2),
1,MCOBPP(2),MCOBPP(2),MBAICO(2),MBAICO(2),MSTEP
I 0027 NO 100 N=1,2
I 0028 IP:NDIPP(N),NO,0.) GO TO 100
I 0029 IP:INSTANT,NO,1) INT=INTOXI(N)
I 0030 NOXID(N)=NOXID(N)/DR*5
I 0031 HALPA(N)=DALPA(N)/DR*5
I 0032 JALPA=HALPA(N)-NOXID(N)
I 0033 IP:(JALPA/2.-GT.MOXID(N)) JALPA=MOXID(N)*2*1
I 0034 INTOXI(N)=1
I 0035 MOA(N)=NOXID(N)-1
I 0036 MBO(N)=NOXID(N)*1
I 0037 MAB(N)=HALPA(N)-1
I 0038 MBA(N)=HALPA(N)/2*1*2
I 0039 GO TO 100
I 0040 IP:(JALPA.-GT.M) GO TO 70
I 0041 INTOXI(N)=2
I 0042 MOA(N)=NOXID(N)-1/2*2
I 0043 MBO(N)=NOXID(N)*2/2*2
I 0044 MAB(N)=(HALPA(N)-1)/2*2
I 0045 MBA(N)=(HALPA(N)*5)/4*4
I 0046 GO TO 100

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158 0043      70 IP:JALPA.GT.32) GO TO 80
159 0045      INTOR(K)=8
160 0046      MOA(K)=(MOXID(K)-2)/808
161 0047      MAO(K)=(MOXID(K)+5)/808
162 0048      MAB(K)=(MALPA(K)-2)/808
163 0049      MDA(K)=(MALPA(K)+11)/808
164 0050      GO TO 100
165 0051      80 IP:JALPA.GT.64) GO TO 90
166 0053      INTOR(K)=8
167 0054      MOA(K)=(MOXID(K)-4)/808
168 0055      MAO(K)=(MOXID(K)+11)/808
169 0056      MAB(K)=(MALPA(K)-4)/808
170 0057      MDA(K)=(MALPA(K)+23)/16014
171 0058      GO TO 100
172 0059      90 INTOR(K)=16
173 0060      MOA(K)=(MOXID(K)-8)/16016
174 0061      MAO(K)=(MOXID(K)+23)/16016
175 0062      MAB(K)=(MALPA(K)-8)/16016
176 0063      MDA(K)=(MALPA(K)+87)/32032
177 0064      100 IP:(NDIPP(1)+NDIPP(2).GT.0.) .AND. (N.RQ.2)) GO TO 101
178 0066      INTB2=INTOR(K)
179 0067      GO TO 108
180 0068      101 IP:INTOR(K).LT.INTOR(K+1) INTB=2*INTOR(K+1)
181 0070      IP:INSTART.NE.1) GO TO 190
182 0071      IP:INTOR(K)-INTI.600.190.400
183 0072      I=1:IMB2-MBA1).LE.(400*INTI) GO TO 190
184 0073      IP:(NDIPP(1)+NDIPP(2).GT.0.) GO TO 190
185 0074      ML=MBA1+10*INT
186 0075      MM=ML-1000)/40000+1
187 0076      LN=PI*MM
188 0077      IP:(NDIPP(2).GT.0.) LN=MBA2-18*INT
189 0078      IP:(M.RGT.LM) MM=LN
190 0079      SLOPE=C(MI)-C(MH)/(R(ML)-P(MH))
191 0080      ML=ML-10*INTB)/INTB+INTB+1
192 0081      TV(ML,RQ,MI) ML=ML*INTB
193 0082      505 MM=MM-INTB
194 0083      DO 510 L=ML,MM,INTB
195 0084      C(L)=C(ML)-SLOPE*(R(ML)-R(L))
196 0085      IP:(M+INTB.RQ.LM) GO TO 190
197 0086      ML=MM*INTB
198 0087      520 MM=ML+64
199 0088      IP:(M.RGT.LM) MM=LN
200 0089      SLOPE=C(MI)-C(MH)/(R(ML)-P(MH))
201 0090      ML=ML*INTB
202 0091      GO TO 505
203 0092      530 LN=MBA2-18*INT
204 0093      LL=MBA2-10*INTB
205 0094      ML=(LL-1)/8000+1
206 0095      IP:(ML.LT.1) ML=1
207 0096      GO TO 520
208 0097      400 INT=INTOR(K)
209 0098      INT2=INT/2
210 0099      IP:(RQ.2) GO TO 150
211 0100      IP:(INT.GT.1) GO TO 105
212 0101      ML=2
213 0102      MM=MC(MOA(K)-1)-1
214 0103      DO 102 L=ML,MM,2
215 0104      C(L)=0.9*(C(L-1)+C(L+1))
216 0105
217 0106
218 0107
219 0108
220 0109
221 0110
222 0111
223 0112
224 0113
225 0114
226 0115

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138 0116 NL=MC:NOA(1)+1) *1
139 0117 NR=MC:(NAB(1)-1) *1
140 0118 DO 103 L=NL,NN,2
141 0119 C(L)=0.5*(C(L-1)+C(L+1))
142 0120 GO TO 130
143 0121 NR=MC:NOA(1)-1)-INT
144 0122 DO 110 L=1,NN,INT
145 0123 C(L+INT/2)=0.5*(C(L)+C(L+INT))
146 0124 NL=MC:NOA(1)+1)
147 0125 NR=MC:(NAB(1)-1)-INT
148 0126 DO 120 L=NL,NN,INT
149 0127 C(L+INT/2)=0.5*(C(L)+C(L+INT))
150 0128 IP=INDIPP(2),GT,0.) GO TO 190
151 0129 NL=MC:(NAB(1)+1)
152 0130 NR=NP:INR-INTB
153 0131 GO TO 159
154 0132 IP=INDIPP(1),GT,0.) GO TO 151
155 0133 NL=1
156 0134 GO TO 155
157 0135 NL=MC:(NAB(1)+1)
158 0136 NR=MC:(NAB(2)-1)-INTB
159 0137 DO 160 L=NL,NN,INTB
160 0138 C(L+INT)=0.5*(C(L)+C(L+INTB))
161 0139 IP=IN,GT,0.) GO TO 165
162 0140 IP=INT,GT,0.) GO TO 165
163 0141 NL=MC:(NAB(2)+1)+1
164 0142 NR=NP:INR-1
165 0143 DO 162 L=NL,NN,2
166 0144 C(L)=0.5*(C(L-1)+C(L+1))
167 0145 NR=NP:INR-1
168 0146 DO 163 L=NL,NN,2
169 0147 C(L)=0.5*(C(L-1)+C(L+1))
170 0148 GO TO 170
171 0149 NL=MC:(NAB(2)+1)
172 0150 NR=MC:NOA(2)-1)-INT
173 0151 DO 170 L=NL,NN,INT
174 0152 C(L+INT/2)=0.5*(C(L)+C(L+INT))
175 0153 NL=MC:NOA(2)+1)
176 0154 NR=NP:INR-INT
177 0155 DO 180 L=NL,NN,INT
178 0156 C(L+INT/2)=0.5*(C(L)+C(L+INT))
179 0157 CONTINUE
180 0158 IP=INDIPP(1),GT,0.) GO TO 300
181 0159 IP=INSTART,NE,1) GO TO 300
182 0160 INTPOL=INTPOL(1)
183 0161 IP=INTPOL,GT,1) INTPOL=INTPOL/2
184 0162 NR=NOA(1)
185 0163 NA=NP:INTPOL
186 0164 IP=(NA),LT,NOXID(1)) GO TO 220
187 0165 C(MA)=C(MP)-(R(MP)-R(MA))*C:(M1)-CUR(1)) / (R(MP)-R(MA))
188 0166 NA=NA+INTPOL
189 0167 GO TO 210
190 0168 NR=NOA(1)
191 0169 NA=NP-INTPOL
192 0170 IP=(NA),GT,NOXID(1)) GO TO 260
193 0171 C(MA)=CAO(1)-(NOXID(1)-R(MA))*CAO(1)-C(MP)) / (NOXID(1)-R(MP))
194 0172 NA=NA-INTPOL
195 0173
196 0174
197 0175
198 0176
199 0177
200 0178
201 0179
202 0180
203 0181
204 0182

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ISN 0187      GO TO 230
ISN 0188      240 NP=NAB1
ISN 0189      NA=NP+INTPOL
ISN 0190      240 IP(R(NA).LT.PALPA(1)) GO TO 260
ISN 0191      C(NA)=C(NP)-P(NP)-R(NA))*C(NP)-CAB(1))/(R(NP)-PALPA(1))
ISN 0192      NA=NA+INTPOL
ISN 0193      GO TO 250
ISN 0194      240 NP=NBA1
ISN 0195      NA=NP-INTOXI(1)
ISN 0196      270 IP(R(NA).GT.PALPA(1)) GO TO 280
ISN 0197      C(NA)=CBA(1)-(PALPA(1)-R(NA))*(CBA(1)-C(NP))/(PALPA(1)-P(NP))
ISN 0198      NA=NA-INTOXI(1)
ISN 0199      GO TO 270
ISN 0200      280 NOXID1=NOXID(1)+1
ISN 0201      NALPA1=NALPA(1)+1
ISN 0202      NOA1=NOA(1)+1
ISN 0203      NAO1=NAO(1)+1
ISN 0204      NAB1=NAB(1)+1
ISN 0205      N9A1=N9A(1)+1
ISN 0206      IF(N9A1PP(2).EQ.0.) GO TO 400
ISN 0207      300 IP(INSTART.NR.1) GO TO 300
ISN 0208      INTPOL=INTOXI(2)
ISN 0209      IF(INTPOL.GT.1) INTPOL=INTPOL/2
ISN 0210      NP=NOA2
ISN 0211      NA=NP-INTPOL
ISN 0212      310 IP(R(NA).GT.NOXID(2)) GO TO 320
ISN 0213      C(NA)=C(NP)-P(NA)-R(NP))*C(NP)-COA(2))/(NOXID(2)-R(NP))
ISN 0214      NA=NA-INTPOL
ISN 0215      GO TO 310
ISN 0216      320 NP=NAO2
ISN 0217      NA=NP+INTPOL
ISN 0218      330 IP(R(NA).LT.NOXID(2)) GO TO 340
ISN 0219      C(NA)=CAO(2)+(R(NA)-NOXID(2))*(CAO(2)-C(NP))/(NOXID(2)-R(NP))
ISN 0220      NA=NA+INTPOL
ISN 0221      GO TO 330
ISN 0222      340 NP=NAB2
ISN 0223      NA=NP-INTPOL
ISN 0224      350 IP(R(NA).GT.PALPA(2)) GO TO 360
ISN 0225      C(NA)=C(NP)-P(NA)-R(NP))*C(NP)-CAB(2))/(PALPA(2)-R(NP))
ISN 0226      NA=NA-INTPOL
ISN 0227      GO TO 350
ISN 0228      360 NP=NBA2
ISN 0229      NA=NP+INTOXI(2)
ISN 0230      370 IP(R(NA).LT.PALPA(2)) GO TO 380
ISN 0231      C(NA)=CBA(1)+(R(NA)-PALPA(2))*(CBA(2)-C(NP))/(PALPA(2)-P(NP))
ISN 0232      NA=NA+INTOXI(2)
ISN 0233      GO TO 370
ISN 0234      390 NOXID2=NPXNE-NOXID(2)
ISN 0235      NALPA2=NPXNE-NALPA(2)
ISN 0236      NOA2=NPXNE-NOA(2)
ISN 0237      NAO2=NPXNE-NAO(2)
ISN 0238      NAB2=NPXNE-NAB(2)
ISN 0239      N9A2=NPXNE-N9A(2)
ISN 0240      400 PRINTN
ISN 0241      END
ISN 0242
ISN 0243
ISN 0244
ISN 0245
ISN 0246

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C
158 0002 SUBROUTINE INTDIP
158 0003 IN INTDIP THE CONCENTRATIONS INTEGRATION IS PERFORMED
158 0004 IMPLICIT REAL8 (A-H,O-S)
158 0005 COMMON/RESNET/ R(1000),OXID(2),WALL,OXID(2),DALPA(2),DR
158 0006 COMMON/TEMP / T(1000),TOXID(2),TALPA(2),TSTART,TSTEAM(2),TWALL(2)
158 0007 COMMON/TEMPIN/ TCOOL(100,2),STCOOL(100,2),THAD(100,2),STRAB(100,2)
158 0008 COMMON/HEAT / HVER(100),HCOOL(2),SBAEA(2),HEATPL(2),OPTRED(2),
158 0009 .OSPLIT,HCAP(100),HSTREAM(2),HRAIDA(2)
158 0010 .OSBPP(2),OCOR(2),ORAB(2),OREACT(2)
158 0011 COMMON/HEA DLM/ HTIAS(20)
158 0012 COMMON/CONCN/ C(1000),COXID(2),CORAL(2),CALDET(2),CBETA(2),
158 0013 OXIGPL(2),HDIOP(2),CSTART,DATM(2)
158 0014 OCAP(500),OVER(500),OTMAX(500)
158 0015 COA(2),CAO(2),CAB(2),CBA(2)
158 0016 OCAPOL(2),OCAPAO(2),OCAPAB(2),OCAPBA(2)
158 0017 COMMON/UNIT / TIME,TRAX,DTTEMP,DTDIPP,DTPRIN,DTMAX(100)
158 0018 HTEMP,HDIOP,HPRINT
158 0019 COMMON/RESH /MOROS,RTINE,HOXID(2),MOX(2)
158 0020 HLEMS,HSTART,WALPA(2)
158 0021 COMMON/RESNET/NT(100),HTCOOL(2),HTWALL(2),HTCOOL(2),HTWALL(2),HGER
158 0022 COMMON/RES HCO/HC(500),HRAHE,HRES,HRA(2),HAB(2)
158 0023 HRA(2),HAB(2),HAB(2),HBA(2),INTOX(2),INTD
158 0024 HOA1,HOA2,HAB1,HBA1,HOXID1,WALPA1
158 0025 HOA2,HAO2,HAZ2,HBA2,HOXID2,WALPA2
158 0026 COMMON/HARPRO/ DENSI,DEWFO,OSTOCH,OXICOR,DEWFA7,FICPAC,OXHEAT
158 0027 COMMON/PROFIL/ CO(500),OLAYER(2),ALAYER(2),BLAYER,OXID(2),
158 0028 2H1,H2,H3,H4,H5,HNUMBER,HECALF
158 0029 COMMON/HINPOT/ HBIYIN(100,2),TIMBIF(100,2),HCOEPP(100,2),
158 0030 HCOEPP(100,2),HABCO(100,2),TRABCO(100,2),
158 0031 OPTLIX(100,2),TQPLIX(100,2),TINSTR(100),DTMIB(100),
158 0032 HBIYIN(2),HDIPIIN(2),KQPLIX(2),WQPLIX(2),
158 0033 HCOEPP(2),HABCO(2),HABCO(2),HSTEP
158 0034 DIMENSION CH(1000)
158 0035 DTM=DTDIPP
158 0036 IP=HDIOP(1)+.07-0.1 GO TO 1100
158 0037 RL=1
158 0038 OVER(1)=0.
158 0039 GO TO 1200
158 0040 RL=2
158 0041 HR=HOA(1)-1
158 0042 DO 1150 L=RL,RR
158 0043 OPTMAX(2)=OCAP(2)/(OVER(L)+OVER(L+1))
158 0044 IP(OTMAX(2)+L-1,DTM) DTM=OPTMAX(L)
158 0045 CONTINUE
158 0046 IP(ML,GT,2) GO TO 1160
158 0047 RL=HOA(1)+1
158 0048 HR=HAB(1)-1
158 0049 GO TO 1110
158 0050 RL=HAB(1)+1
158 0051 IP(HDIOP(2)+GT,0.) GO TO 1200
158 0052 IP(HR,DO,HRES) GO TO 1300
158 0053 OVER(HRES+1)=0.
158 0054 HR=HRES
158 0055 GO TO 1110
158 0056
158 0057
158 0058
158 0059
158 0060
158 0061
158 0062
158 0063

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134 0044      1200  NH=HAB(2)-1
135 0045      1210  DO 1250 L=NL,NH
136 0046          OBTMAX(L)=OCAP(L),OVER(L),OVER(L+1)
137 0047          IF(OBTMAX(L).LT.DTH) DTH=OBTMAX(L)
138 0048      1250  CONTINUE
139 0049          IF(NH.EQ.HDES-1) GO TO 1399
140 0050          IF(NH.EQ.HOA(2)-1) GO TO 1250
141 0051          NL=HAB(2)+1
142 0052          NH=HOA(2)-1
143 0053          GO TO 1210
144 0054      1260  NL=HOA(2)+1
145 0055          NH=HDES-1
146 0056          GO TO 1210
147 0057      1300  IF(DTH.NE.DTSTPP) GO TO 1320
148 0058          NH=1
149 0059          GO TO 1350
150 0060      1320  DTH=0.99DTH
151 0061          NH=OBTSTPP/DTH+1.
152 0062          NH=NHMAX
153 0063          DTH=DTSTPP/NHMAX
154 0064          IF(DTH.GT.0. ) GO TO 1350
155 0065          WRITE(6,1236)
156 0066      1236  FORMAT(10,30)TIME STEP 0
157 0067          WRITE(6,5151) HOA(1),HAB(1),HOA(2),HOA(1),HAB(1),HAB(2),HOA(1),HAB(1),HAB(1),HAB(1),
158 0068          1  HBA2,HAB2,HAB2,HOA2,HDES,  (MC(L),L=1,HDES)
159 0069      5151  FORMAT(1H,20F5)
160 0070          1  HDES), (OBTMAX(L),L=1,HDES)
161 0071      5252  FORMAT(1H,10D13.3)
162 0072          NH=HDES
163 0073          NH=URN
164 0074      1350  IF(NDIIPP(1).EQ.0.) GO TO 1370
165 0075          C(1)=C(MC(2)),NDIIPP(1),OR(1),OVER(2)
166 0076          IF(C(1).GT.ORIGCON) C(1)=ORIGCON
167 0077          ORIGPL(1)=C(1)-C(MC(2)),OVER(2)/P(1)
168 0078          OA1=C(HOA(1))-COA(1),OVER(HOA(1))
169 0079          AO1=C(HO(1))-C(HA(1)),OVER(HOA(1)+1)
170 0080          AB1=C(HAB(1))-C(HBA(1)),OVER(HAB(1)+1)
171 0081          BA1=C(HA(1))-C(HBA(1)),OVER(HAB(1)+1)
172 0082          C(MPIR)=C(MC(HR)),NDIIPP(2),OR(MPIR)/OVER(HDES)
173 0083          IF(C(MPIR).GT.ORIGCON) C(MPIR)=ORIGCON
174 0084          ORIGPL(2)=C(MPIR)-C(MC(HR)),OVER(HDES-1),OVER(HDES)/P(MPIR)
175 0085          OA2=C(HOA(2))-COA(2),OVER(HOA(2)+1)
176 0086          AO2=C(HO(2))-C(HA(2)),OVER(HOA(2))
177 0087          AB2=C(HAB(2))-C(HBA(2)),OVER(HAB(2)+1)
178 0088          BA2=C(HA(2))-C(HBA(2)),OVER(HAB(2)+1)
179 0089          DO 2000 K=1,NHMAX
180 0090          1360  IF(NDIIPP(1).GT.0.) GO TO 1400
181 0091          NL=2
182 0092          CH(1)=C(1)+OVER(2)+C(MC(2))-C(1)+DTH/OCAP(1)
183 0093          GO TO 1500
184 0094      1800  NL=2
185 0095          NH=HOA(1)-2
186 0096          CH(HOA(1))=C(HOA(1))+OVER(HOA(1)-1)+C(MC(HOA(1)-2))-C(HOA(1))-C(1)
187 0097          1  DTH/OCAP(HOA(1)-1)
188 0098          GO TO 1450
189 0099      1810  IF(NL.GT.NH) GO TO 1450
190 0100          DO 1450 L=NL,NH

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150 0170      N=MC:L
150 0171      CH(N)=C(N) * (OVER(L) * (C(MC(L-1)) - C(N))
1          * (OVER(L+1) * C(MC(L+1)) - C(N)) * BTM/OCAP(L)
150 0172      1500 CONTINUE
150 0173      IF(ML.GT.2) GO TO 1460
150 0174      NL=MOA(1) * 2
150 0175      NH=HAB(1) * 2
150 0176      CH(MO1) = C(MO1) * (A01-OVER(MO1) * 2) * C(MO1) - C(MC(MO1) * 2))
150 0177      1          * BTM/OCAP(MO1) * 1)
1          * C(HAB1) - C(MO1) * (A02-OVER(MO1) * 2) * C(MO1) - C(MO1) - AB1)
1          * BTM/OCAP(MO1) * 1)
150 0178      GO TO 1410
150 0179      NL=HAB(1) * 2
150 0180      CH(MO1) = C(MO1) * (DA1-OVER(HAB(1) * 2) * C(MO1) - C(MC(HAB(1) * 2))
1          * BTM/OCAP(HAB(1) * 1)
1          * BTM/OCAP(HAB(1) * 1)
1          * (MR.MO.NHES) GO TO 1500
1          * NH=HAB
1          * OVER(MO1) * 1)
1          * C(HAB1) * 1
150 0181      GO TO 1410
150 0182      NH=HAB(2) * 2
150 0183      CH(MO2) = C(MO2) * (A02-OVER(MO2) * 2) * C(MO2) - C(MC(MO2) * 2))
1          * BTM/OCAP(MO2) * 1)
1          * BTM/OCAP(MO2) * 1)
150 0184      GO TO 1510
150 0185      NL=ML
150 0186      CH(N) = C(N) * (OVER(L) * (C(MC(L-1)) - C(N))
1          * (OVER(L+1) * C(MC(L+1)) - C(N)) * BTM/OCAP(L)
150 0187      1550 CONTINUE
1550 0188      1555 IF(MR.MO.NHES-1) GO TO 1400
150 0189      IF(MR.MO.MO(2)-2) GO TO 1560
150 0190      NL=HAB(2) * 2
150 0191      NH=MOA(2) * 2
150 0192      CH(MO2) = C(MO2) * (A02-OVER(MO2) * 2) * C(MO2) - C(MC(MO2) * 2) - AB2)
1          * BTM/OCAP(MO2) * 1)
1          * BTM/OCAP(MO2) * 1)
1          * C(MO2) * (A02-OVER(MO2) * 2) * C(MO2) - C(MC(MO2) * 2))
1          * BTM/OCAP(MO2) * 1)
150 0193      GO TO 1510
150 0194      NL=MOA(2) * 2
150 0195      CH(MO2) = C(MO2) * (OVER(MO2) * 2) * C(MC(MO2) * 2) - C(MO2) - CA2)
1          * BTM/OCAP(MO2) * 1)
150 0196      GO TO 1510
150 0197      NL=1
150 0198      NH=HAB
150 0199      IF(MO1PP(1).NE.0.) NL=2
150 0200      IF(MO1PP(2).NE.0.) NH=HAB-1
150 0201      DO 1700 L=NL,NH
150 0202      N=MC:L
150 0203      C(N) = C(N)
150 0204      1700 CONTINUE
150 0205      2000 RETURN
150 0206      END

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194 0162

3000 WRITE(J,3000)
    FORMAT(140,20,OUTSIDE ALPHA LAYER )
    NA=N1+1
    IY=IL-LS,NAAB(1) GO TO 1210
    WRITE(J,300) NC(NAAB(1)),NC(NAAB(1))
    WRITE(J,600) X(N1),Z(N2)
    WRITE(J,400) Y(N2),TALPA(1)
    WRITE(J,500) CO(NA),CO(N2)
    GO TO 1260
1210 NN=NAAB(1)-1
    WRITE(J,300) NC(INOA(1)),INC(N1),K=NL,NH),NC(NAAB(1))
    WRITE(J,600) X(N1),K=NA,N2)
    WRITE(J,400) Y(N2),TALPA(1),T(INC(N1)),K=NL,NH),TALPA(1)
    WRITE(J,500) CO(N1),K=NA,N2)
1260 NL=NAAB(1)+1
    NA=N2+1
    NN=NA+12
    NA=1000
    IY=(NDIPP(2).50-0.1) GO TO 1300
    IZ=NP-02,NAZ) NP=NGES
    IY=NY-02,N3) N3=N3
    WRITE(J,4500)
    WRITE(J,300) NC(NAAB(1)),INC(N1),K=NL,NH)
    WRITE(J,600) X(N1),K=NA,N2)
    WRITE(J,400) Y(N2),TALPA(1),T(INC(N1)),K=NL,NH)
    WRITE(J,500) CO(N1),K=NA,NH)
    IZ=NP-50,NAZ) GO TO 3000
1400 NL=NP+1
    NP=NL+12
    NA=N2+1
    NN=NA+12
    IZ=NP-02,NAZ) GO TO 2000
    IY=NP-02,NGES) NP=NGES
    IY=NY-02,N3) N3=N3
    WRITE(J,4500)
    WRITE(J,300) NC(N1),K=NL,NH)
    WRITE(J,600) X(N1),K=NA,N2)
    WRITE(J,400) Y(N2),T(INC(N1)),K=NL,NH)
    IZ=NP-50,NAZ) GO TO 5000
    GO TO 1400
1500 NL=NAAB(1)+1
    NN=NAAB(2)-1
    NA=N2+1
    WRITE(J,4500)
    WRITE(J,300) NC(NAAB(1)),INC(N1),K=NL,NH),NC(NAAB(2))
    WRITE(J,600) X(N1),K=NA,N2)
    WRITE(J,400) Y(N2),TALPA(1),T(INC(N1)),K=NL,NH),TALPA(2)
    WRITE(J,500) CO(N1),K=NA,N2)
    GO TO 1500
2000 NN=NAZ-1
    IZ=(NDIPP(1)) 2050,2050,2100
2050 NA=NL
    NN=N1
    GO TO 2150

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13M 0163
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13M 0214
13M 0215
13M 0216
13M 0217
13M 0218
13M 0219
13M 0220
13M 0221

2100 WRITE(J,3500)
2150 WRITE(J,300)
      (MC(H),R=RL,MH),MC(MAB(2))
      (X(E),R=HA,HE)
      (T,MC(H),R=HL,MH),TALPA(2)
      (CO(H),R=HA,HE)
2200 ML=MAB(2)+1
      *P(MOZPP(1)) 2002,2002,2003
2002 VA=V1+1
      ME=M2
      GO TO 2005
2003 VA=M3+1
      ME=M3
2005 WRITE(J,4000)
4000 POBRAT(180,204)INSIDE ALPHA LAYER
      *P(ML,L=MOA(2)) GO TO 2210
      WRITE(J,300) MC(MAB(2)),MC(MOA(2))
      WRITE(J,400) X(MA),X(ME)
      WRITE(J,400) TALPA(2),TOXID(2)
      WRITE(J,450) CO(MA),CO(ME)
      GO TO 2222
2210 MH=MOA(2)-1
      WRITE(J,300) MC(MAB(2)),MC(H),R=HL,MH),MC(MOA(2))
      WRITE(J,400) X(M),R=MA,ME)
      WRITE(J,400) TALPA(2),T( MC(H)),R=HL,MH),*OXID(2)
      WRITE(J,450) CO(H),R=HA,HE)
2222 ML=MOA(2)+1
2250 MA=M2+1
      ME=M1
      GO TO 2300
2260 MA=M3+1
      ME=M5
2300 WRITE(J,3500)
1400 POBRAT(180,204)INSIDE OXIDE LAYER
      WRITE(J,300) MC(MOA(2)),MC(H),R=HL,MH),
      WRITE(J,400) X(M),R=MA,ME)
      WRITE(J,400) TOXID(2),T( MC(H)),R=HL,MH),RQFS)
      WRITE(J,450) CO(H),R=HA,HE)
4000 IF(MPLOT.EQ.0) RETURN
      MPLOT = 01
      *P( 5 OF VARIABLES AS FUNCTION OF "IMP. HAVE TO BE MADE
      MPLOT=MPLOT+1
      PLO(10,MPLOT)=0.
      PLO(20,MPLOT)=0.
      PLO( 1,MPLOT)=SM2(TIME)
      PLO( 2,MPLOT)=SM2(TSTEAR(1))
      PLO( 3,MPLOT)=SM2(TSTEAR(1))
      PLO(11,MPLOT)=SM2(TSUBP(2))
      PLO(12,MPLOT)=SM2(TWALL(2))
      PLO(13,MPLOT)=SM2(TSUBP(2))
      PLO(14,MPLOT)=SM2(TSUBP(2))
      PLO(15,MPLOT)=SM2(TSUBP(2))
      PLO( 4,MPLOT)=SM2(TWALL(1))
      PLO( 5,MPLOT)=SM2(TSUBP(1))
      PLO( 6,MPLOT)=SM2(OLAYER(1))
      PLO( 7,MPLOT)=SM2(ALAYER(1))
      PLO( 8,MPLOT)=PLO( 6,MPLOT)+PLO( 7,MPLOT)
      PLO( 9,MPLOT)=PLO( 6,MPLOT)+PLO( 8,MPLOT)
      PLO(10,MPLOT)=SM2(OXID(1))
      PLO(11,MPLOT)=PLO( 8,MPLOT)+2

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15N 0222
:SN 0223
15N 0224
15N 0225
15N 0226
15N 0227
15N 0228
15N 0229
15N 0230
15N 0231
15N 0232
15N 0233
15N 0234
:SN 0235
15N 0236

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PLO:13,KPLOT)=PLO:10,KPLOT)002
PLO:16,KPLOT)=SMG:(OLAYER:2)
PLO:17,KPLOT)=SMG:(ALAYER:2)
PLO:18,KPLOT)=PLO:16,KPLOT)+PLO:17,KPLOT)
PLO:19,KPLOT)=PLO:16,KPLOT)/PLO:18,KPLOT)
PLO:20,KPLOT)=SMG:(ODAIN:3)
PLO:21,KPLOT)=PLO:18,KPLOT)002
PLO:22,KPLOT)=PLO:20,KPLOT)002
PLO:23,KPLOT)=PLO:20,KPLOT)+PLO:10,KPLOT)
CDAVRS=.00100833/(RALPA(1)002-PALPA(2)002)002.0R(1)
PFRM=0.0001*DIATER/WALL
PLO:25,KPLOT)=PFRM
RETURN
END

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12W 0002 SUBROUTINE PREPAR
12W 0003 THE RESULTS ARE PREPARED FOR PRINTING AND PLOTTING
12W 0004 IMPLICIT REAL8 (A-H,O-Z)
12W 0005 COMMON/COMMON/ B(1000), BOXID(2), DALPA(2), WALL, BOXID(2), DALPA(2), DR
12W 0006 / T(1000), TOXID(2), DALPA(2), TSTART, TSTEADY(2), TWALL(2)
12W 0007
12W 0008 1, TSTEP(2)
12W 0009 COMMON/COMMON/ TCOOL(100,2), STCOOL(100,2), TRAP(100,2), STRAD(100,2)
12W 0010 / NVER(100), MCOOL(2), SHAD(2), MSHAP(2), OXID(2), OXID(2),
12W 0011 / OXID(2), MSHAP(100), MSHAP(2), MSHAP(2), MSHAP(2)
12W 0012 1
12W 0013 2
12W 0014 COMMON/COMMON/ COOL(2), COOL(2), COOL(2), COOL(2), COOL(2),
12W 0015 / COOL(2), COOL(2), COOL(2), COOL(2), COOL(2), COOL(2),
12W 0016 / COOL(2), COOL(2), COOL(2), COOL(2), COOL(2), COOL(2),
12W 0017 / COOL(2), COOL(2), COOL(2), COOL(2), COOL(2), COOL(2),
12W 0018 / COOL(2), COOL(2), COOL(2), COOL(2), COOL(2), COOL(2),
12W 0019 / COOL(2), COOL(2), COOL(2), COOL(2), COOL(2), COOL(2),
12W 0020 / COOL(2), COOL(2), COOL(2), COOL(2), COOL(2), COOL(2),
12W 0021 / COOL(2), COOL(2), COOL(2), COOL(2), COOL(2), COOL(2),
12W 0022 / COOL(2), COOL(2), COOL(2), COOL(2), COOL(2), COOL(2),
12W 0023 / COOL(2), COOL(2), COOL(2), COOL(2), COOL(2), COOL(2),
12W 0024 / COOL(2), COOL(2), COOL(2), COOL(2), COOL(2), COOL(2),
12W 0025 / COOL(2), COOL(2), COOL(2), COOL(2), COOL(2), COOL(2),
12W 0026 / COOL(2), COOL(2), COOL(2), COOL(2), COOL(2), COOL(2),
12W 0027 / COOL(2), COOL(2), COOL(2), COOL(2), COOL(2), COOL(2),
12W 0028 / COOL(2), COOL(2), COOL(2), COOL(2), COOL(2), COOL(2),
12W 0029 / COOL(2), COOL(2), COOL(2), COOL(2), COOL(2), COOL(2),
12W 0030 / COOL(2), COOL(2), COOL(2), COOL(2), COOL(2), COOL(2),
12W 0031 / COOL(2), COOL(2), COOL(2), COOL(2), COOL(2), COOL(2),
12W 0032 / COOL(2), COOL(2), COOL(2), COOL(2), COOL(2), COOL(2),
12W 0033 / COOL(2), COOL(2), COOL(2), COOL(2), COOL(2), COOL(2),
12W 0034 / COOL(2), COOL(2), COOL(2), COOL(2), COOL(2), COOL(2),
12W 0035 / COOL(2), COOL(2), COOL(2), COOL(2), COOL(2), COOL(2),
12W 0036 / COOL(2), COOL(2), COOL(2), COOL(2), COOL(2), COOL(2),
12W 0037 / COOL(2), COOL(2), COOL(2), COOL(2), COOL(2), COOL(2),
12W 0038 / COOL(2), COOL(2), COOL(2), COOL(2), COOL(2), COOL(2),
12W 0039 / COOL(2), COOL(2), COOL(2), COOL(2), COOL(2), COOL(2),
12W 0040 / COOL(2), COOL(2), COOL(2), COOL(2), COOL(2), COOL(2)

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M=MC(M)
CO(M)=C(M)
18 X(M)=XOUT-R(M)
M=MAB(2)
X(M1)=BLAYER
CO(M1)=CBA(2)
X(M1)=BLAYER
CO(M1)=CAB(2)
M=MAB(2)*
M=MAB(2)*
DO 19 M=RL,M
M=MC(M)
CO(M)=C(M)
19 X(M)=XOUT-R(M)
M2=MOA(2)*
CO(M2)=CAO(2)
X(M2)=XOUT-ROHID(2)
ALAYER(2)=BALPA(2)-ROHID(2)
X(M2)=X(M2)
CO(M2)=COA(2)/PICPAC
M=MORH
M2=MOA(2)*
XOUT=R(1)+ROHID(2)*PICPAC-1
DO 20 M=1,M
M=MC(M)
CO(M)=C(M)/PICPAC
X(M)=XOUT-R(M)*PICPAC
OALPHA(2)=ROHID(2)*PICPAC
OALPHA(2)=OALPHA(2)+OALPHA(2)*OALPHA(2)
GO TO 60
25 M=MOA(1)*
OALPHA(1)=ROHID(1)*PICPAC
XOUT=R(1)+ROHID(1)*PICPAC-1
DO 26 M=1,M
M=MC(M)
CO(M)=C(M)/PICPAC
X(M)=XOUT-R(M)*PICPAC
M=MAB(1)
CO(M1)=COA(1)/PICPAC
X(M1)=ROHID(1)
CO(M1)=CAO(1)
ALAYER(1)=ROHID(1)-BALPA(1)
BLAYER=BALPA(1)-R(MPINE)
XOUT=R(1)
M=MOA(1)*
M=MAB(1)*
DO 27 M=RL,M
M=MC(M)
CO(M)=C(M)
27 X(M)=XOUT-R(M)
M2=MOA(1)*
X(M2)=BALPA(1)
CO(M2)=CAB(1)
X(M2)=X(M2)
CO(M2)=CBA(1)
  
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150 0133 NL=HAB (1);+1
150 0134 IP (NDIPP (2)) 20.20.29
150 0135 M3=HDS+2
150 0136 M=HDS
150 0137 GO TO 30
150 0138 M3=HAB (2)+2
150 0139 M=HAB (2)-1
150 0140 X (M3)=R (1)-BALPA (2)
150 0141 BLAYER=ALPA (1)-BALPA (2)
150 0142 CO (M3)=CBA (2)
150 0143 DO 31 M=NL,MM
150 0144 M=MC (M)
150 0145 CO (M+2)=C (M)
150 0146 X (M+2)=R (1)-S (M)
150 0147 OTOTAL=OXID (1)+ALPA (1)+BETA
150 0148 ODAIN (1)=DAIN (1)
150 0149 IP (NDIPP (2)).W0.0.1 GO TO 40
150 0150 X (M3+1)=X (M3)
150 0151 CO (M3+1)=CAB (2)
150 0152 M=HQA (2)+3
150 0153 M=HAB (2)+1
150 0154 M=HQA (2)-1
150 0155 DO 33 M=NL,MM
150 0156 M=MC (M)
150 0157 X (M+3)=R (1)-S (M)
150 0158 CO (M+3)=C (M)
150 0159 X (M)=R (1)-BOXID (2)
150 0160 CO (M+1)=CNO (2)
150 0161 X (M+1)=X (M)
150 0162 CO (M+1)=COA (2)/PICPAC
150 0163 HOUTR (1)+BOXID (2)+ (PICPAC-1)
150 0164 M=HQA (2)+1
150 0165 M=HDS
150 0166 M=HDS+4
150 0167 DO 34 M=NL,MM
150 0168 M=MC (M)
150 0169 X (M+4)=HOUT-S (M)+PICPAC
150 0170 CO (M+4)=C (M)/PICPAC
150 0171 ALYER (2)=ALPA (2)-BOXID (2)
150 0172 CLAYER (2)=BOXID (2)+PICPAC
150 0173 OTOTAL=OTOTAL+ALPA (2)+OXID (2)
150 0174 ODAIN (2)=DAIN (2)+ (M3INE)/R (1)
150 0175 GO TO 200
150 0176 ODAIN=0.50;BOXID (1)+2-BOXID (2)+2)+CSTART/RRPRAD
150 0177 BLAYER=BOXID (1)-BOXID (2)
150 0178 ALYER (1)=0.
150 0179 CLAYER (2)=0.
150 0180 OTOTAL=OETA
150 0181 IP (NDIPP (1)).W0.0.1 GO TO 100
150 0182 X (M3+1)=X (M3)+2-BOXID (1)+2)+OXICCN/RRPRAD
150 0183 OTOTAL=OTOTAL+OXID (1)
150 0184 ODAIN (1)=DAIN (1)
150 0185 BLAYER (1)=OXID (1)+PICPAC
150 0186 IP (NDIPP (2)).W0.0.1 GO TO 200
150 0187 ODAIN (2)=0.50;BOXID (2)+2- (M3INE)+2)+OXICCN/RRPRAD
150 0188 OTOTAL=OTOTAL+OXID (2)
150 0189 ODAIN (2)=DAIN (2)

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129 0219 OLAVER (2) = DOLIB (2) * PICPAC
130 0218 DO 300 K=1,3
131 0217 IP (NDI PP IN) = 0.0
132 0216 OLAVER (1) = OLAVER (4) * 10000.
133 0215 ALAVER (1) = ALAVER (1) * 10000.
134 0214 COORD (1) = COORD (1) * 1000.
135 0213 CALPA (1) = CALPA (1) * 1000.
136 0212 OGAIS (1) = OGAIS (1) * 1.00.
137 0211 CONTINUE
138 0210 OLAVER = OLAVER * 10000.
139 0209 OGAIS = OGAIS * 1000.
140 0208 OTOTAL = OTOTAL * 1000.
141 0207 IP (RSTART = 0.0) OGAIS = OTOTAL
142 0206 RETURN
143 0205 END

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129 0219
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ISM 0002      C
ISM 0003      DIPCON DIPCON (T1, T2, C1, C2, K)
ISM 0004      DIFFUSION CONSTANT ( CM=2/SEC)
ISM 0005      IMPLICIT REAL*8 (A-H,O-S)
ISM 0006      COMMON/MATPBO/ DENSIB, DENSIM, OSTOCH, OIICOM, DENRAT, PICPAC
ISM 0007      TH=0.5*(T1+T2)+273.16
ISM 0008      IP (TH, 67.2135.) TH=2125.
ISM 0009      R=1.987
ISM 0010      RTM=RTM
ISM 0011      CM=.5*(C1+C2)
ISM 0012      GO TO (1, 2, 3), K
ISM 0013      1 DIPCON=0.6711*DEXP(-33600./RTM)
          C DIPCON=PICPAC*2 = DIP.CONST.OP IFO2
          RETURN
ISM 0014      2 DIPCON=5.200*DEXP(-50000./RTM)
ISM 0015      3 DIPCON = DIP.CONST.OP ALPHA SINCALCY
          RETURN
ISM 0016      3 DIPCON=0.053*DEXP(-28200./RTM)
ISM 0017      3 DIPCON = DIP.CONST.OP BETA SINCALCY
ISM 0018      RETURN
ISM 0019      END

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ISH 0002      C      SUBROD TIME INT PAC (T, CH, CL, H)
ISH 0003      EQUILIBRIUM CONCENTRATION AT THE INTERFACES (GRAM OXYGEN/CM**3)
ISH 0004      IMPLICIT REAL*8 (A-M, O-S)
ISH 0005      COMMON/NATPRO/ DENSI, DENSM, OSTOCH, OXICON, DENRAT, PICFAC
ISH 0006      TR=1.273.16
ISH 0007      IPTR=65.2125.) TR=2125.
ISH 0008      GO TO (I, 2) A
ISH 0009      1 CH=1.517-7.5E-5*TH
ISH 0010      CH=CM*PICFAC
ISH 0011      C      CH/PICFAC = CONCENTRATION AT OXIDE/ALPHA INTERFACE
ISH 0012      CL=0.0699*DENSI
ISH 0013      C      CL = CONCENTRATION AT ALPHA/OXIDE INTERFACE
ISH 0014      RETURN
ISH 0015      2 IPTR=17.1123.16) TR=1123.16
ISH 0016      CM=1.0.127302*TR*1.5931E-4-TR**2*3.901E-9)*DENSI
ISH 0017      C      CM = CONCENTRATION AT ALPHA/BETA INTERFACE
ISH 0018      IPTR=1273.16) 3, 3, 0
ISH 0019      C      CL = CONCENTRATION AT BETA/ALPHA INTERFACE
ISH 0020      RETURN
ISH 0021      3 CL=0.82263*DEXP(-14995.2/(1.497*TH))*DENSI
            C      CL = CONCENTRATION AT BETA/ALPHA INTERFACE
            RETURN
            END

```

```

ISH 0002          FUNCTION SPEC(S,K)
ISH 0003          VOL.SPEC.HEAT (MSFC/(CH*3000))
ISH 0004          IMPLICIT REAL*8 (A-N,O-Z)
ISH 0005          COMMON/HATPBO/ DENZIN,DEHNO,OSTOCH,OXICON,DEHMAT,PICPAC
ISH 0006          TR=1.273.16
ISH 0007          IP(TR.GT.2123.) TR=2123.
ISH 0008          GO TO (1,2),K
ISH 0009          1 SPEC=0.549*TR*6.79-5
ISH 0010          SPEC=SPEC*DEHNO*PICPAC
ISH 0011          SPEC./PICPAC = SPEC.HEAT OF SRO2
ISH 0012          RETURN
ISH 0013          2 IP(TR=1000.) 3,3,N
ISH 0014          3 SPEC=.2409*1.689*OTR-0.360*OTR**2
ISH 0015          SPEC = SPEC.HEAT OF ZIRCALOY
ISH 0016          GO TO 5
ISH 0017          4 SPEC=.3653
ISH 0018          IP (TR.GT. 1123.16) .AND. (TR.LT. 1223.16)
ISH 0019          5 SPEC=.3653*0.6595*DSIN(3.14159*(TR-1123.16)/100.)
ISH 0020          SPEC = SPEC.HEAT OF ZIRCALOY
          RETURN
          END

```

```

ISM 0002      C      FUNCTION CONDUCT(T2,T3,R)
ISM 0003      C      THERMAL CONDUCTIVITY (W/(CM*CI))
ISM 0004      C      IMPLICIT= SPAL08 (A-N,O-Z)
ISM 0005      C      COMMON/ATPRO/ DENZIR,DEHMO,OSTOCH,CRICOM,DEMPAT,PICPIC
ISM 0006      C      TR=50 (T1+T2)+273.16
ISM 0008      C      TP=TR-07.3125, TR=3125.
ISM 0009      C      GO TO (1,2),R
ISM 0010      C      1 CONDUC=0.52
ISM 0011      C      CONDUC=CONTRC/PICVAC
ISM 0012      C      CONDUC=PICPAC * CONDUCT.OF 1R02
ISM 0013      C      RETURN
ISM 0014      C      2 CONDUC=-0.0876*TR*2.75D-4
ISM 0015      C      CONDUC = CONDUCT.OF BINCALOY
ISM 0016      C      RETURN
ISM 0017      C      END

```

```

ISN 0002      SUBROUTINE DATPLO
C             INPUT DATA FOR PLOTS OF VARIABLES AS FUNCTIONS OF TIME ARE READ
C             AND THE PLOTTING ROUTINE DATPLO IS CALLED
ISN 0003      COMMON/RESULT/PLO(25,200),NPLOT,NPLOT
ISN 0004      COMMON/DATAP/CD(5,200),DYN(4),DYS(4),DXN,DZE,NA(20),NPTV(4)
ISN 0005      COMMON/HEADR/NTITLE(20)
ISN 0006      DIMENSION NPLOT(4)
ISN 0007      DO 75 N=1,NPLOT
ISN 0008      READ(5,300) NPLOTX,DXN,DZE,NVAR,IPLOT,V00,(NTITLE;N),N=16,20)
ISN 0009      300 FORMAT(I10,2E10.4,2I10,E10.4,5A8)
ISN 0010      NA=1
ISN 0011      NZ=5
ISN 0012      DO 10 L=1,NVAR
ISN 0013      READ(5,600) NPLOTY(L),DYN(L),DYS(L),NPTV(L),(NA;N),N=NA,NZ)
ISN 0014      600 FORMAT(I10,2E10.4,I10,20E,5A8)
ISN 0015      NA=NZ+1
ISN 0016      NZ=NA+4
ISN 0017      10 CONTINUE
ISN 0018      DO 50 I=1,NPLOT
ISN 0019      CD(5,I)=PLO(NPLOTX,I)
ISN 0020      DO 50 L=1,NVAR
ISN 0021      CD(L,I)=PLO(NPLOTY(L),I)
ISN 0022      50 CONTINUE
ISN 0023      IF(((IPLOT/2)*2).EQ.IPLOT) GO TO 71
ISN 0024      NHEAD=5*NVAR
ISN 0025      WRITE(6,700) (NTITLE;N),N=1,20),(NA;N),N=1,NHEAD)
ISN 0026      700 FORMAT(1R1,10E,20A8/1R0,9E,9WABSCISSA,9E,20A8)
ISN 0027      DO 70 I=1,NPLOT
ISN 0028      WRITE(6,800) CD(5,I),(CD(L,I),L=1,NVAR)
ISN 0029      800 FORMAT(1R,5E20.5)
ISN 0030      70 CONTINUE
ISN 0031      71 IF((((IPLOT/10)/2)*2).NE.(IPLOT/10))
ISN 0032      1CALL DATPLO(100,NVAR,NPLOT,NTITLE)
ISN 0033      75 CONTINUE
ISN 0034      RETURN
ISN 0035      END
ISN 0036

```

```

15N 0002 SUBROUTINE DATPLO(Y0,NVAR,NX,NY,NT,MTITLE)
15N 0003 COMMON/DATAPCD(5,200),DYN(N),DYE(N),DIM,NX,NY,NA(20),NPTY(N)
15N 0004 DIMENSION PLOT(3000),MTITLE(20),IS(N)
15N 0005
15N 0006 DATA IS/0,1,2,3/
15N 0007 ROUTINE TO PLOT UP TO 4 VARIABLES
15N 0008 SCALE VARIABLES IN ARRAY CD
15N 0009 DYN = NPTS PER INCH
15N 0010 DYE = VALUE AT GRAPH 0
15N 0011 DO 50 L=1,NVAR
15N 0012 SP=1.0/DYN(L)
15N 0013 DO 50 I=1,NT
15N 0014 SP*(CD(L,I) - SP*(CD(L,I) - DYE(I)))
15N 0015
15N 0016 DO 51 I=1,NT
15N 0017 SP*(CD(5,I) - SP*(CD(5,I) - DYE(5)))
15N 0018 PLOT SET UP
15N 0019 SE = 0.14
15N 0020 SN = 0.1
15N 0021 XO = 0.0
15N 0022 YB = Y0 + 0.0
15N 0023 YT = Y0 + 10.0
15N 0024 CALL PLOTX(PLY,3000)
15N 0025
15N 0026 PLOT HEADER
15N 0027 CALL SYMBOL(X0,2.0,0.105,20WR,P,PANPL,NM,P,4500,90.0,0.20)
15N 0028 X = X0 + 1.0
15N 0029 CALL SYMBOL(X,2.0,0.105,MTITLE(1),60.0,80)
15N 0030 XO = X0 + 2.0
15N 0031 LABEL PLOTS
15N 0032
15N 0033 DO 630 L=1,NVAR
15N 0034 IF(L.EQ.1) GO TO 101
15N 0035 DO 100 K=2,1
15N 0036 IF(DYN(L).EQ.DYN(K-1)).AND.(DYE(L).EQ.DYE(K-1)) GO TO 630
15N 0037 100 CONTINUE
15N 0038 101 CONTINUE
15N 0039 X = X0 + 0.08
15N 0040 Y = Y0 + 4.0
15N 0041 CALL SYMBOL(X,Y,SS,IS(L),60.0,-1)
15N 0042 LN = 50L - 8
15N 0043 Y = Y + 0.15
15N 0044 X = Y + 0.04
15N 0045 CALL SYMBOL(X,Y,RH,NA(LN),60.0,20)
15N 0046 LABEL SCALEY
15N 0047 X = X0 + 0.2
15N 0048 Y = Y0 + 0.05
15N 0049 YV = DYE(L)
15N 0050 DO 635 I=1,11
15N 0051 CALL NUMBER(X,RH,RY,0.0,6M(59,I))
15N 0052 Y = Y + 1.0
15N 0053 YV = YV + DYE(I)
15N 0054 635 DRAW VERTICAL LINE
15N 0055 X = X0 + 1.0
15N 0056 CALL PLOT(X,YB,3)
15N 0057 CALL PLOT(X,YT,2)
15N 0058 430 X0 = X

```

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ISM 0049
ISM 0050
ISM 0051
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ISM 0100
ISM 0101
ISM 0102
ISM 0103
ISM 0104
ISM 0105

XV = DXZ
YR = Y00-0.15
XT = X0-0.2
XMIN = X0
XMAX=XMIN
CALL NUMBER(NT, YR, SM, YV, 0.0, 6H(P7.2))
DETERMINE PLOT CONDITIONS FOR 100 PTS PER SECTION
IOV=0
ISTART = 1
ISTOP = 50
600 IF(ISTOP.GT.NT) ISTOP=NT
DO 650 L=1, N(NT)
DO 640 I=ISTART, ISTOP
I = CB(S, 2) + X0
IF(I.GT.XMAX) XMAX=I
Y=CB(L, 1)+Y00
IF(Y.LT.0.0.OR.Y.GT.YT) GO TO 651
IF(Z.EQ.ISTART) GO TO 652
IF(IOR.WO.1) GO TO 652
IF(IPY(L).EQ.0) CALL PLOT(Z, Y, 3)
CALL PLOT(Z, Y, 2)
GO TO 650
651 IOV=1
GO TO 650
652 IOV=0
CALL PLOT(Z, Y, 3)
CALL SYMBOL(X, Y, SS, IS(1), 0.0, -2)
CALL PLOT(Z, Y, 2)
650 CONTINUE
ISTART=ISTOP
IF(ISTART.GE.NT) GO TO 700
ISTOP=ISTOP+50
GO TO 600
700 ISTOP=XMAX-XMIN
NSTOP=IPIX(ISTOP)+1
N=NO
YC=YB+0.25
DO 660 I=1, NSTOP
IX=1.0
YV=XV+DXM
XT=XT+1.0
CALL PLOT(X, YC, 3)
CALL PLOT(X, YB, 2)
CALL PLOT(X, YB, 3)
660 CALL NUMBER(NT, YR, SM, XV, 0.0, 6H(P7.2))
CALL PLOT(X, YB, 2)
IX=X+3.0
CALL PLOT(X, 0.0, -3)
RETURN
END

```


ISH 0002

```
      SUBROUTINE PROFLO
C ** PROGRAM TO CRT PLOT DATA FOR PROGRAM SIMRAN 1, 01-16-74
C ** AUTHOR: ON HESS, UCNC CSD ONNL, PO BOX 1, OAK RIDGE, TN. 37810
C
C ** VARIABLES REQUIRED ARE IN COMMON, PARABOLIC INTERPOLATION IS
C ** DONE BETWEEN ELEMENTS (C(L),L=1,N1), (C(M),M=N1,N2), (C(N),N=N2,N3)
C ** FOR GRAPH TYPE 1, PLUS (C(L),L=N3,N4) AND (C(N),N=N4,N5) FOR
C ** GRAPH TYPE 2 DEPENDING ON NDIPP(1) AND NDIPP(2)=0,0 OR >0,0.
C ** X-AXIS SCALE: IF X(N1)-X(1).GE.0.05CH, 1 INCH = 0.005 CH, TYPE 1,
C **                OR X(N3)-X(1).GE.0.05CH, 1 INCH = 0.005 CH, TYPE 2.
C **                SIMILARLY, IF X(N2)-X(1).LT.0.05CH, 1 INCH = 0.0025CH, TYPE 1,
C **                OR X(N3)-X(1).LT.0.05CH, 1 INCH = 0.0025CH, TYPE 2.
C **                START AND END X-AXIS WITH DIVISION .1T. X(1) AND .0T. X(N1) OR
C **                X(N3).
C ** Y-AXIS SCALE: SAME FOR BOTH GRAPHS, 1 INCH = 0.2 CM/CM**3, TN 0.4
C **                CM/CM**3 DIVISIONS, STARTING WITH 0.
C **                NEW FEATURE: NSCAL = 1, EXPAND Y-RANGE TO 0.0-0.4
C **                INSTEAD OF 0.0-2.0 FOR NSCAL = 0.
C ** LINE INTENSITIES: INCREASE FROM NORM LINES TO 1.4NF FOR X(N)'S TO
C **                X,Y-AXIS TO CURVES OF C VS. X.
C ** N VALUES ARE DETERMINED FROM NDIPP(1).GT.0, NN = N = 1, TYPE1 PLOT,
C **                OR NDIPP(2).GT.0, NN = N = 2, TYPE1 PLOT,
C **                AND N1 = N2 = 1 OR N1 = N2 = 2
C **                FOR TYPE2, NN = N = 1 OR 2, N1 = 1 AND N2 = 2.
C
```

ISH 0003

```
      IMPLICIT REAL*8 (A-H,O-S)
C
C C = CONC., X = DIST., OBLAYE & ALAYER ARE THICKN., OXID & ALFA ARE
C OXYGEN CONTENT, BETA,TOTAL ARE BARE; BETA IS CO; GAIN IS GAIN.
C ADD BLAYER = THICKNESS AND NSCAL = Y-AXIS SCALE FACTOR.
C
```

ISH 0004

ISH 0005

ISH 0006

```
      COMMON/PROVAR/NDIPP(2),CSTART,TIME
      COMMON/HEADLN/NTITL(20)
      COMMON/PROFIL/C(500),X(500),OBLAYER(2),ALAYER(2),BLAYER
      1,OXID(2),ALFA(2),GAIN(2),BETA,TOTAL,BETA0,TEMP
      2,
      N1,N2,N3,N4,N5,MUNPLT,NSCAL
```

ISH 0007

```
      DIMENSION IPLTA(4000),NS(5)
C
C INL,INS,INTA,ICVN ARE BEAM INTENSITIES FOR MESH LINES, X(1)'S,
C X,Y-AXES AND C VS. X.
C DATA IPLTP/0/,NSUP/4000/,INL,INS,INTA,ICVN/1/,14,17,19/
C DATA NIP/10/
C NIP IS NO. OF INTERPOLATED PTS. BETWEEN DATA PTS.
C
```

ISH 0010

ISH 0012

ISH 0013

ISH 0014

ISH 0015

```
      INITIALIZE CRT PLOTTER 1ST TRY ONLY
      IF( IPLTP.EQ.1 ) GO TO 5
      CALL CRT( IPLTA,NSUP,'OURUSS 4540NS',0 )
      IEPP = 0
      IPLTP = 1
      5 CONTINUE
C
C CHECK MUNPLT-- IF NEG. THIS IS FINAL PLOT, SET INTCR2 PND PLOT
C PLO IEPP = 9000 AND MUNPLT TO POS. VALUE.
C IF( MUNPLT.LT.0 ) IEPP = 9000
C IF( MUNPLT.LT.0 ) MUNPLT = - MUNPLT
```

ISH 0016

ISH 0017


```

ISH 0067      XLIM = (XUL-XLL)/XFACT
ISH 0068      NY = ((YUL-YLL)/YDIV) + 1
ISH 0069      NSCAL = 1.0/XFACT
ISH 0070      XOFF = XLL + NSCAL
ISH 0071      DDY = YDIV/XFACT

C
C ** MOVE GRAPH ORIGIN FROM (0.0,0.0) TO (0.5,0.5)
C ** MAKE GRAPH ORIGIN AT Y0 = 1.0 INSTEAD OF 0.5, 02-26-75.
C ** CALL CRT( 0.5,1.0,0.3 )
C
C
C DRAW Y-AXIS VALUES, HEADING
C POP NSCALE = 0, DO Y-RANGE 0.0-2.0 W/PNT P3.1, = 1 DO 0.000-0.500
C   W/PNT P5.3.
C   XY = 0.0
C   YY = -DDY
C   YLAB = -YDIV
C   NGTY = 0.15
C   WPTHY = 0.12
C   DO 30 I = 1,NT
C   YY = YY + DDY
C   YLAB = YLAB + YDIV
C   IF(NSCALE.NE.0)CALL CRTNBR(XY-0.4),YY-0.07,NGTY,YLAB,0,(P3.1)
C   IF(NSCALE.NE.0)CALL CRTNBR(XY-0.6),YY-0.07,NGTY,YLAB,0,(P5.3)
C
C DRAW HORIZONTAL MESH LINES TOWARD THE RIGHT
C   IP( 1,NO.1 ) GO TO 32
C   XG = XY
C   YG = YY
C   CALL CRT( XG,YG,0.1 )
C   XG = XLIM
C   CALL CRT( XG,YG,INT(.1) )
C   XG = XY
C   CALL CRT( XG,YG,0.1 )
C 32 CONTINUE
C   IF( 1,NO.1/2 ) GO TO 30
C   IP( NSCALE,NO.0 ) XH = XY - 0.46
C   IP( NSCALE,NO.0 ) XH = XY - 0.70
C   YH = (YLLIM - 31.0000000) + 0.5
C   CALL CRTSYM( XH,YH,NGTY,ORIGEN CONCENTRATION (OR/CHOO)H,40.0,31)
C 30 CONTINUE

C
C DRAW HEADING ACROSS TOP FROM NTITLE(20) IN CORNER
C   XT = XLIM - 80.0000000 + 0.5
C   YT = YLLIM + 0.15
C   CALL CRTSYM( XT,YT,NGTY,NTITLE(1),0.0,80 )
C
C DRAW TOP AXES BACK TO LEFT, THEN DOWN TO ORIGIN.
C   CALL CRT( XLLIM,0.1 )
C   CALL CRT( X0,YLLIM,XVA,1 )
C   CALL CRT( X0,Y0,XHA,1 )
C   CALL CRT( X0,Y0,0.1 )
C
C DRAW X-AXIS VALUES, HEADING ALONG BOTTOM
C   XI = -DDX
C   YI = Y0 - 0.25
C   NGIX = 0.15
C   XLAB = XLL - XDIV
C   WPTHX = 0.12

```

```

ISH 0116 DO 60 I = 1, NR
ISH 0117 XE = X + DD
ISH 0118 XLAB = XLAB + XDIV
ISH 0119 CALL CPTDR( XE-0.36, YH, NGTX, XLAB, 0.0, 0.0, (P6.3) )
C
C DRAW VERTICAL MESH LINES UP AT EACH X-AXIS DIV., TOWARD THE RIGHT
IP = 1.80, 1 ) GO TO #2
YV = YX
YV = Y0
CALL CRT( XE, YV, 0.1 )
YV = YLTH
CALL CRT( XE, YV, 0.1 )
YV = Y0
CALL CRT( XE, YV, 0.1 )
#2 CONTINUE
IP( Y, NR, NR/2 ) GO TO #0
XN = XLIN - 81.0*DBDTHX) * 0.5
YH = Y0 - 0.50
CALL CRTSR( XN, YH, NGTX, DISTANCE FROM OPTIMAL OUTER SURFACE (CM),
1, 0, 0, 0.1 )
#0 CONTINUE
C
C DRAW X-AXIS FROM RIGHT BACK TO ORIGIN.
CALL CRT( XLIN, Y0, 0.1 )
CALL CRT( X0, Y0, XTRA, 1 )
CALL CRT( X0, Y0, 0.1 )
C
C DRAW VERTICAL X (1), -- X (NR) FROM LEFT TO RIGHT, NS(1), (NR) = N1, NR
C FOR TIER 1 OR 2, NL = NC + 1 = N OF 6 VERTICAL LINES
C XOFF IS DISTANCE (IN.) ALL IS OFFSET FROM 0,0, NEG. OR POS.
NL = NC + 1
DO 50 L = 1, NL
NV = 1
IF( L.GT.1 ) NV = NS(L-1)
XV = X(NV) * XSCAL - XOFF
YV = Y0
CALL CRT( XE, YV, 0.1 )
YV = YLTH
CALL CRT( XE, YV, 0.1 )
YV = Y0
CALL CRT( XE, YV, 0.1 )
#0 CONTINUE
C
C PREPARE TO PLOT C VS. X, DO 3 OR 5 CURVES, NM = NS(3) OR NS(5)
C NA IS 1ST INDEX AND IS RESET TO VALUE OF 2ND INDEX FOR NEXT CURVE.
C ** FOR NSCAL > 0, Y-AXIS RANGE = 0.0 - 0.1, ONLY ANY C VALUES > 0.1
C ** MODIF. TO INTERPOLATE BETWEEN DATA POINTS. 01-30-74.
NIP = NIP
NMI = NIP-1
NA = 1
DO 60 I = 1, NC
IND1 = 1
ND = NS(I)
NP = NB-NA+1
DO 65 M = 1, NP
NMI = M-1
IP = X(NMI)*NSCAL - XOFF

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```

ISM 0163 VP = C*(N1)*YSICAL - YOPP
ISM 0164 IP( VP,DT,VLIN ) GO TO 65
C POSITION BEAN AT 1ST POINT OF EACH CURVE.
ISM 0166 CALL CRT( XP,YP,0.1 )
ISM 0167 IP( MP,LE,2 ) GO TO 64
ISM 0168 IND1 = IND1 + 1
ISM 0169 DX = (X(N) - X(NM1))/PHIP
ISM 0170 X' = X(NM1)
ISM 0171 DO 63 N = 1,MN1
ISM 0172 X' = X(N) + DX
ISM 0173 X' = X(N) + DX
ISM 0174 YI = YLAG( XI,X(MA),C(MA),IND1,3,MP,IPX )
ISM 0175 XP = X*YSICAL - YOPP
ISM 0176 YP = Y*YSICAL - YOPP
ISM 0177 IP( VP,DT,VLIN ) GO TO 63
ISM 0178 CALL CRT( XP,YP,ICVX,1 )
ISM 0179 63 CONTINUE
ISM 0180 64 CONTINUE
ISM 0181 XP = X(N)*YSICAL - YOPP
ISM 0182 YP = C(N)*YSICAL - YOPP
ISM 0183 IP( VP,DT,VLIN ) GO TO 65
ISM 0184 CALL CRT( XP,YP,ICVX,1 )
ISM 0186 65 CONTINUE
ISM 0187 YP( 2,LT,MC ) NA = NB + 1
ISM 0188 60 CONTINUE
ISM 0190 REST: NA TO NB + 1 FOR NEXT CURVE EXCEPT APTTP LAST CURVE.
C
C
C ADD START VS X(1),---X(NM) IN DASHED LINE FROM X(1) TO X(M).
ISM 0191 X1 = X(1)*YSICAL - YOPP
ISM 0192 X4 = X(N)*YSICAL - YOPP
ISM 0193 V1 = C*ARTWYSICAL - YOPP
ISM 0194 DEL = 0.25
ISM 0195 DEB = 0.12
ISM 0196 CALL CRT( X1,V1,0.1 )
ISM 0197 X1 = DMC1( X1,DEL,XM )
ISM 0198 CALL CRT( X1,V1,ICVX,1 )
ISM 0199 X1 = DM1( X1,DEB,XM )
ISM 0200 CALL CRT( X1,V1,0.1 )
ISM 0201 IP( X1,LT,XN ) GO TO 67
C
C
C DRAW LEGEND AT RIGHT END OF GRAPH
C FOR TYPE1, K = 1 OR 2, DEPENDING ON MDEFP(1) OR (2)>0, K1=M2ER.
C FOR TYPE2, K = 2 FOR DRAWING ARRAY VALUES, K1 = 1, K2 = 2.
C DRAW LEGEND FROM TOP DOWNWARD, LINE 1 = TIME
ISM 0203 XX = VLIN + 0.5
ISM 0204 YV = VLIN - 0.25
ISM 0205 DY = 0.25
ISM 0206 VP = XX
ISM 0207 VP = YV
ISM 0208 CALL CRTSYM( XR,YR,HGTX,TEMP,1,0.0,5 )
ISM 0209 XR = XR + 5.0*DM1X
ISM 0210 YR = YR + 5.0*DM1X
ISM 0211 CALL CRTSYM( XR,YR,HGTX,TEMP,0.0,(M) )
ISM 0212 XR = XR + 4.0*DM1X
ISM 0213 CALL CRTSYM( XR,YR,HGTX,TEMP,0.0,8 )
C
C ** DRAW LINE 2 = TEMP, RESET X, INCREASE Y BY DY
C ** MAKE MORE SPACE BETWEEN TIME AND T = TEMP, 00-24-74.
ISM 0214 XR = XX

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ISM 0215      YR = YR - 2.0*DY
ISM 0216      CALL CRTSYM( XR,YR,NGTX,'Z',.0,0.3 )
ISM 0217      XR = XR + 3.0*WDTHX
ISM 0218      ITEMP = ITEMP
ISM 0219      CALL CRTSYM( XR,YR,NGTX,ITEMP,0.0,'(Z)' )
ISM 0220      XR = XR + 4.0*WDTHX
ISM 0221      CALL CRTSYM( XR,YR,NGTX,'DEG.C',0.0,6 )

C
C ** DRAW LINES 3,6 LAYER THICKNESS AND MICRONS)
C ** MAKE MORE SPACE BETWEEN T = TEMP AND LAYER THICKNESS, 02-20-75.
ISM 0222      YR = YR - 2.0*DY
ISM 0223      XR = XR
ISM 0224      CALL CRTSYM( XR,YR,NGTX,'LAYER THICKNESS',0.0,15 )
ISM 0225      YR = YR + DY
ISM 0226      CALL CRTSYM( XR,YR,NGTX,' (MICRONS)',0.0,12 )

C
C ** DRAW LINES 5 - 8 FROM OLAYER, ALAYER ARRAYS, K1,K2 = 1,2, IF TYPE 2.
ISM 0227      YR = YR - DY
ISM 0228      XR = XR
ISM 0229      CALL CRTSYM( XR,YR,NGTX,'ZMO',0.0,4 )
ISM 0230      XR = XR + 4.0*WDTHX
ISM 0231      DO 70 K = K1,K2
ISM 0232      CALL CRTSYM( XR,YR,NGTX,OLAYER(K),0.0,'(P9.1)' )
ISM 0233      YR = YR + DY
ISM 0234      70 CONTINUE

C
C **
ISM 0235      XR = XR
ISM 0236      CALL CRTSYM( XR,YR,NGTX,'ALPHA',0.0,6 )
ISM 0237      XR = XR + 6.0*WDTHX
ISM 0238      DO 75 K = K1,K2
ISM 0239      CALL CRTSYM( XR,YR,NGTX,ALAYER(K),0.0,'(P7.1)' )
ISM 0240      YR = YR + DY
ISM 0241      75 CONTINUE

C
C ** DRAW LINE 6A FOR BETA FROM FLAYER, ADDED 01-22-75.
ISM 0242      YR = YR - DY
ISM 0243      CALL CRTSYM( XR,YR,NGTX,'BETA',0.0,5 )
ISM 0244      XR = XR + 5.0*WDTHX
ISM 0245      CALL CRTSYM( XR,YR,NGTX,FLAYER,0.0,'(P8.1)' )

C
C ** DRAW LINES 9,10, OXYGEN CONTENT & (MG/CM**2)
C ** MAKE MORE SPACE BETWEEN BETA AND OXYGEN CONTENT, 02-20-75.
ISM 0246      YR = YR - 2.0*DY
ISM 0247      XR = XR
ISM 0248      CALL CRTSYM( XR,YR,NGTX,'OXYGEN CONTENT',0.0,14 )
ISM 0249      YR = YR + DY
ISM 0250      CALL CRTSYM( XR,YR,NGTX,' (MG/CM**2)',0.0,12 )

C
C ** DRAW LINES 11,(12), FROM OXID(1),(2) AS ZMO(1),(2)
ISM 0251      YR = YR - DY
ISM 0252      CALL CRTSYM( XR,YR,NGTX,'ZMO',0.0,4 )
ISM 0253      XR = XR + 4.0*WDTHX
ISM 0254      DO 80 K = K1,K2
ISM 0255      CALL CRTSYM( XR,YR,NGTX,OXID(K),0.0,'(P9.2)' )
ISM 0256      YR = YR + DY
ISM 0257      80 CONTINUE

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C      DRAW LINE(S) 13,(14) FROM ALPHA(1),(2) AS ALPHA(1),(2)
ISN 0259      XR = XX
ISN 0260      CALL CRTSYN( XR,YR,NGTX,'ALPHA ',0.0,6 )
ISN 0261      XR = XR + 6.0*WDTX
ISN 0262      DO 85 K = R1,K2
ISN 0263      CALL CRTNUM( XR,YR,NGTX,ALPHA(K),0.0,'(P7.2)' )
ISN 0264      YR = YR - DY
ISN 0265      85 CONTINUE

C
C      DRAW LINE 15 FOR BETA
ISN 0266      XR = XX
ISN 0267      CALL CRTSYN( XR,YR,NGTX,'BETA ',0.0,5 )
ISN 0268      XR = XR + 5.0*WDTX
ISN 0269      CALL CRTNUM( XR,YR,NGTX,BETA,0.0,'(P8.2)' )

C
C      DRAW LINE 16 FROM TOTAL
ISN 0270      XR = XX
ISN 0271      YR = YR - DY
ISN 0272      CALL CRTSYN( XR,YR,NGTX,'TOTAL ',0.0,6 )
ISN 0273      XR = XR + 6.0*WDTX
ISN 0274      CALL CRTNUM( XR,YR,NGTX,TOTAL,0.0,'(P7.2)' )

C
C      DRAW LINE 17 FROM BETAS AS CO
ISN 0275      XR = XX
ISN 0276      YR = YR - DY
ISN 0277      CALL CRTSYN( XR,YR,NGTX,'CO ',0.0,3 )
ISN 0278      XR = XR + 3.0*WDTX
ISN 0279      CALL CRTNUM( XR,YR,NGTX,BETAS,0.0,'(P10.2)' )

C
C      DRAW LINE 18 FROM GAIN
C ** DRAW GAIN(K) VALUE(S), 02-24-75.
ISN 0280      XR = XX
ISN 0291      YR = YR - DY
ISN 0282      CALL CRTSYN( XR,YR,NGTX,'GAIN ',0.0,5 )
ISN 0283      XR = XR + 3.0*WDTX
ISN 0284      DO 90 K = R1,K2
ISN 0285      CALL CRTNUM( XR,YR,NGTX,GAIN(K),0.0,'(P8.2)' )
ISN 0286      90 YR = YR - DY

C
C      DRAW PLOT NUMBER FROM HUMPLT
C      NUMBER LOOKS LIKE-- 012275001 (I9 FORMAT)
C ** DRAW HUMPLT AT LOWER RIGHT, SAME LEVEL AS X-AXIS HEADING, 02-24-75.
ISN 0287      XPH = XX + 4.0*WDTX
ISN 0288      YPH = Y0 - 0.5
ISN 0289      CALL CRTNUM( XPH,YPH,NGTY,HUMPLT,0.0,'(I9)' )

C
C      TERMINATE EACH GRAPH, ADVANCE FILM
C ** CHECK INTEGER END PLOT FLAG IEPP-- IF = 9000, THIS IS FINAL PLOT.
ISN 0290      XNU = 0.0
ISN 0291      YNU = 0.0
ISN 0292      CALL CRT( XNU,YNU,IEPP,2 )

C
ISN 0293      RETURN
ISN 0294      END

```

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