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Preliminary Outline for Book:

Engineering for Nuclear Reactor Fuel Reprocessing

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November 15, 1957

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FOREWORD

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1.0

The outline in its present form represents the state of our thinking at an arbitrary cut-off date of October 15, 1957, and makes no pretense of completeness or elegance.

2.0

Reference to particular sites, and in some instances the inclusion of registered trade marks, was done as a memory aid for the subsequent use of the writers and should not be expected to find such prominence in the finished manuscript.

3.0

Certain chapters have been classified "Confidential" to avoid any suggestion of security violation. As writing progresses it is likely that more and more of the material will have to be so treated, and no attempt at declassification will be made until the package is finished. It should be understood that only material believed to be declassifiable will be included in the text.



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Chapter Synopses

	Preface	
I	Introduction	20 pages
п	Special Considerations in Radiochemical Processing	30 pages
	Shielding	
	Criticality	
	Maintenance	
	Waste Disposal	
III	Chemical Processes	75 pages
	BiPO	
	Redox	
	"25" Process	
	Purex	
	Thorex	
	Miscellaneous Processes	
IV	Chemical Operations	60 pages
	Dissolution	
	Oxidation - Reduction	
	Electrolysis	
	Precipitation and Crystallization	
V	Mechanical Operations	45 pages
	Agitation	
	Centrifugation	
	Filtration (liquid-solid)	
	Filtration (gas -liquid and gas -solid)	
	Fluidization	
	Physical Treatment	
VI	Fluid Flow	45 pages
	Piping and Pipe Connections	
	Pumps	
	Valves	

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VII Heat Transfer Operations

Heat Transfer Without Change of Phase Boiling and Evaporation Vapor Condensation Calcination

VIII Solvent Extraction

Introduction Mixer-Settlers Pulse Columns Other Conventional Equipment Other Unconventional Equipment De-emulsification

IX Other Mass Diffusion Operations

Gas-liquid Absorption Adsorption Drying Ion Exchange Distillation and Recitfication Steam Stripping

X Instrumentation

General Désign Considerations Measurements Control and Read-out

XI Auxiliary Equipment

Carriers Viewing Devices Manipulators Samplers

XII Plant Design

Process Design Project Design Hazards Study Plant Start-up 45 pages

45 pages

105 pages

30 pages

30 pages

90 pages

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XIII Plant Operation

Management Operations Analytical Operations SS Accountability Health Physics Plant Protection Maintenance Utilities Stores

XIV Fuel Cycle Economics

30 pages

The Nuclear Fuel Cycle

Chemical Reprocessing in the Nuclear Fuel Cycle Economic Comparison of Various Fuel Reprocessing Methods Factors Affecting Reprocessing Costs 30 pages

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Outline for

PREFACE

- 1.0 Need for Book
- 2.0 Object of Book
- 3.0 Scope of Book
 - 3.1 Definition of Chemical Reprocessing

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- 3.2 What It Covers
- 3.3 What It Does Not Cover
- 4.0 Acknowledgments

Outline for Chapter I

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INTRODUCTION

and any data that has been any one from

1.0 Nuclear Fuel Reprocessing

2.0 Problems Associated with Chemical Reprocessing

3.0 History of Chemical Reprocessing

4.0 Trends in Chemical Reprocessing

1.0 Nuclear Fuel Reprocessing

1.1 Fuel Requirements for Energy Needs

1.1.1 Present

1.1.2 Projected

Fig: Energy needs for the future

1.2 Place of Nuclear Fuels in Future Energy Production

1.3 Nuclear Fuel Cycle

Fig: Nuclear fuel cycle

1.4 Need for Chemical Reprocessing

2.0 Problems Associated with Chemical Reprocessing

2.1 Radioactivity

2.1.1 Health hazard

2.1.2 Material damage

2.1.3 Remote operation

2.1.4 Equipment decontamination

2.1.5 Waste disposal

2.2 Criticality

2.3 Heavy Isotope Build-Up and Effect

2.4 Chemical Problems

2.4.1 Product specifications

2.4.2 Low losses

2.4.3 Diversity and intractability of materials

Table:Reactor fuel elements and cladding materialsTable:Bonding agents for reactor fuel elementsTable:Chemical forms of reactor fuels

3.0 History of Chemical Reprocessing

- 3.1 Pu Recovery for Military Use
- 3.2 Valuable Uranium in Process Wastes
- 3.3 Evolution of Reprocessing Methods
 - 3.3.1 Precipitation
 - 3.3.2 Solvent extraction

4.0 Trends in Chemical Reprocessing

- 4.1 Shorter-Cooled Materials
- 4.2 Volatility
- 4.3 Pyrometallurgical Reprocessing
- 4.4 Ion Exchange
- 4.5 New Solvents

Outline for Chapter II

SFECIAL CONSIDERATIONS IN RADIOCHEMICAL FROCESSING

- 1.0 Introduction
- 2.0 Shielding
- 3.0 Criticality
- 4.0 Maintenance
- 5.0 Waste Disposal

1.0 Introduction

2.0 Shielding

2.1 Introduction and Theory

2.1.1	α	Fig.:	Range of Alpha Particles
2.1.2	β	Fig.:	Energy Spectrum of Beta Emission
2.1.3	γ	Fig.:	Range of Beta Particles in Several Materials

- a. Point source, line source, volume source
- b. Exponential attenuation

Fig.: Exponential Attenuation of Gamma Rays b

2.1.4 Neutrons

2.2 Materials

- 2.2.1 Desirable properties
 - a. Heavy mass
 - (1) Relation to absorption coefficient

Table: Gamma Ray Absorption Coefficients of Several Materials

- b. Inexpensive
- c. Practicable
- 2.2.2 Typical materials
 - a. Lead
 - b. Concrete
 - c. Water
 - d. Earth
 - e. Iron
 - f. Barytes
- 2.3 Methods
 - 2.3.1 Cells
 - 2.3.2 Unit shielding
 - 2.3.3 Underwater
- 2.4 Typical Examples

3.0 Criticality

- 3.1 Introduction and Theory
 - 3.1.1 Reflected or unreflected
- 3.2 Geometry Control

Fig.: Critical Concentration vs. Diameter of Cylinder

- 3.3 Batch Control
- 3.4 Dilution Control
- 3.5 Typical Calculations
- 4.0 Maintenance
 - 4.1 Introduction

- 4.1.1 Statement of problem
- 4.1.2 Need pointed out
- 4.1.3 Amelioration through design
 - a. Ease of decontamination
 - b. Reliability as related to moving parts
 - c. Ease of removal

4.2 Types of Maintenance

- 4.2.1 Direct
 - a. Description
- 4.2.2 Remote
 - a. Description
- 4.2.3 Underwater
 - a. Description

5.0 Waste Disposal

- 5.1 Statement of Problem
 - 5.1.1 Health hazard
 - 5.1.2 Nature of radioactivity
 - a. Decay can't be altered
 - 5.1.3 Heat dissipation
- 5.2 Troublesome Activities
 - 5.2.1 Relation to age of waste
- 5.3 Chemical Nature of Waste
 - 5.3.1 Process vs. composition
 - 5.3.2 Corrosiveness
- 5.4 Low Level Waste

5.4.1 Solid

a. Disposal by burial

5.4.2 Liquid

a. Holdup for decay

b. Disposal by dilution

c. Concentration by evaporation

5.4.3 Gas

a. Disposal by dilution

5.5 High Level Wastes

5.5.1 Solid

a. Disposal by burial

5.5.2 Liquid

a. Indifinite storage in underground tanks

(1) Corrosion problem

(2) Toxicity (radio and chemical)

(3) Heat liberation

(4) Cost

5.5.3 Gas

a. Pressure storage

(1) Process description

(2) Problems

(3) Cost

Outline for Chapter III

CHEMICAL PROCESSES

- 1.0 Introduction
- 2.0 BiPO Process
- 3.0 Redox Process
- 4.0 "25" Process
- 5.0 Purex Process
- 6.0 Thorex Process
- 7.0 Miscellaneous Processes

1.0 Introduction

- 1,1 Scope of Chapter
- 1.2 Chronology Chart of Processes: BiPO₄, Redox, "25", Purex, Thorex, and Volatility

Fig: Chronology of Chemical Reprocessing Methods for Spent Reactor Fuels

2.0 BiPO, Process

- 2.1 Introduction
 - 2.1.1 History
 - 2.1.2 Object and need of process
 - 2.1.3 Scope of process
 - 2.1.4 Advantages and disadvantages of process
 - 2.1.5 Site employing process
 - 2.1.6 Present status
- 2.2 Process Characteristics

Fig: Solubilities of Pu compounds

- 2.2.2 Characteristics of U (as affecting BiPOh process)
- 2.2.3 Fission products

Table: Important fission products in chemical reprocessing

Fig: Solubility of various fission products

- 2.2.4 Theory of coprecipitation
- 2.2.5 Theory of carriers
- 2.2.6 Theory of scavengers
- 2.3 Process Description

2.3.1 Flowsheet

Fig: Simplified flowsheet of BiPOL process

- 2.3.2 Feed preparation
- 2.3.3 Extraction
- 2.3.4 Decontamination
- 2.3.5 Concentration (or cross-over)
 - a. Valence adjustment to Pu+6
 - b. BiPO by-product precipitation
 - c. LaF3 by-product precipitation
 - d. LaF3 product precipitation
 - e. Metathesis of LaF3 product precipitate
 - f. Product purification
- 3.0 Redox Process
 - 3.1 Introduction

3.1.1 History

3.1.2 Purpose and need of process

3.1.3 Scope of process

3.1.4 Specifications on final product

3.1.5 Advantages and disadvantages of process

3.1.6 Site employing process

3.1.7 Present status

3.2 Process Characteristics

3.2.1 Reasons for choice of nitrate system

3.2.2 Characteristics of U as affecting Redox process

Fig: Solubility of UO2(NO3)2 in aqueous and Hexone systems

Fig: Uranium distribution between organic and aqueous

phases

3.2.3 Characteristics of Pu as affecting Redox process

Fig: . Flutonium distribution between organic and

aqueous phases

3.2.4 Characteristics of fission products as affecting Redox process

Fig: F. P. distribution between organic and aqueous

phases

3.2.5 Description of solvent and properties

Table: Physical properties of Hexone

3.2.6 Description of feed material and properties

Table: Physical properties of feed

3.2.7 Solvation

3.2.8 Salting

3.2.9 Acid and acid-deficient operation

3.3 Process Description

3.3.1 Flowsheet

Fig: Simplified flowsheet of Redox process

3.3.2 Feed preparation

3.3.3 Extraction

a. Description of extraction step

b. Valence adjustment

c. Extraction variables

Fig: Effect of temperature on Redox extraction

d. Decontamination factor

Fig: Column equilibrium diagram

e. U losses

f. Pu losses

g. Column equilibrium diagrams

3.3.4 Partition of U and Pu

a. Description of partition step

b. Valence adjustment

c. Partition variables

Fig: Effect of temperature on Redox partitioning

d. Decontamination factor

e. U losses

f. Pu losses

g. Column equilibrium diagrams

Fig: Column equilibrium diagram

3.3.5 Uranium decontamination (2nd U cycle)

a. Description of steps

b. Decontamination variables

cycle

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c. Column equilibrium diagram

Fig: Column equilibrium diagram

d. Function of 2D column

Fig: Column equilibrium diagram

e. Function of 2E column

Fig: Column equilibrium diagram

f. U losses

3.3.6 Plutonium decontamination (2nd Pu cycle)

- a. Description of steps
- b. Decontamination variables
- c. 2A column equilibrium diagram

Fig: Column equilibrium diagram

d. Function of 2B column

Fig: Column equilibrium diagram

- e. Pu product concentration
- f. Pu losses

3.3.7 Al(NO3)3 recovery

- a. Description of process
 - (1) Flowsheet

Fig: Simplified flowsheet of Al(NO3)3 recovery

system

3.3.8 Hexone recovery

- a. Description of process
- b. Flowsheet

Fig: Simplified flowsheet of Hexone recovery

c. Hexone losses

3.3.9 Waste disposal

a. Liquid wastes

b. Gaseous wastes

4.0 "25" Process

- 4.1 Introduction
 - 4.1.1 History
 - 4.1.2 Purpose and need of process
 - 4.1.3 Scope of process
 - 4.1.4 Specifications on final product
 - 4.1.5 Advantages and disadvantages of process
 - 4.1.6 Site employing process
 - 4.1.7 Present status

4.2 Process Characteristics

4.2.1 Use of a nitrate acid-deficient system

4.2.2 Characteristics of U as affecting "25" process

Table: Distribution coefficients and separation

factors

4.2.3 Pu behavior in "25" process

4.2.4 Characteristics of fission products as affecting "25" process

Table: F. P. distribution between Hexone and

aqueous phases

4.2.5 Description of feed materials and properties

Table: Physical properties of feed

4.3 Process Description

4.3.1 Flowsheet

Fig: Simplified flowsheet of "25" process

4.3.2 Feed preparation

Table: Composition of dissolver offgas

4.3.3 Extraction and stripping operations

a. Description of operations

b. First cycle operations

c. Intercycle evaporation

d. Second cycle operations

Fig: Effect of temperature on second cycle opera-

tions

Fig: Column equilibrium diagram

e. Third cycle operations

Fig: Effect of temperature on third cycle opera-

tions

Fig: Column equilibrium diagram

4.3.4 Solvent recovery

Fig: "25" process solvent recovery flowsheet

a. Sources of contaminated solvent

b. Caustic scrub

c. Distillation

d. Losses

4.3.5 Waste disposal

a. Aqueous waste

b. Gaseous waste

Fig: "25" process offgas flowsheet

4.3.6 Criticality considerations

- 5.0 Purex Process
 - 5.1 Introduction
 - 5.1.1 History
 - 5.1.2 Purpose and need of process
 - 5.1.3 Scope of process
 - 5.1.4 Specifications on final product
 - 5.1.5 Advantages and disadvantages of process
 - 5.1.6 Site employing process
 - 5.1.7 Present status
 - 5.2 Process Characteristics
 - 5.2.1 Reasons for use of nitrate system
 - 5.2.2 Characteristics of U as affecting Purex process

Table: Distribution of U between TBP and aqueous

phases

5.2.3 Characteristics of Pu as affecting Purex process

Table: Distribution of Pu between TBP and aqueous

phases

5.2.4 Characteristics of fission products as affecting Purex process

Table: Distribution of F. P.'s between TBP and

aqueous phases

5.2.5 Description of solvent and properties

Table: Physical properties of TBP

5.2.6 Description of feed material and properties

Table: Fhysical properties of feed

- 5.3 Process Description
 - 5.3.1 Flowsheet

Fig: Simplified flowsheet of Purex process

5.3.2 Feed preparation

5.3.3 Extraction

- a. Description of extraction step
- b. Valence adjustment

Table: Distribution coefficients for U and Pu

c. Extraction variables

Fig: Effect of temperature on extraction

- d. Decontamination factor
- e. U losses
- f. Pu losses
- g. Column equilibrium diagrams

Fig: Column equilibrium diagram

5.3.4 Partition of U and Pu

- a. Description of partition step
- b. Valence adjustment
- c. Partition variables

Fig: Effect of temperature on partition of U and Pu

- d. Decontamination factor
- e. U losses
- f. Pu losses
- g. Column equilibrium diagrams

5.3.5 Uranium decontamination (2nd U cycle)

- a. Description of steps
- b. Salting effect of HNO2

c. Decontamination variables

Fig: Effect of temperature on Uranium decontamina-

tion

- d. Function of 2D column
- e. Function of 2E column
- f. Product U concentration

g. Decontamination factor

h. U losses

i. Column equilibrium diagrams

Fig: Column equilibrium diagram

5.3.6 Plutonium decontamination (2nd Pu cycle)

- a. Description of steps
- b. Valence adjustment
- c. Decontamination variables
- d. Function of 2B column
- e. Equilibrium diagram for 2A and 2B column
 - Fig: Column equilibrium diagrams

f. Pu product concentration

g. Decontamination factor

h. Pu losses

5.3.7 Solvent recovery

a. Description of process

b. TBP product specifications

Fig: Simplified flowsheet for solvent recovery

5.3.8 Acid recovery

- a. Reasons for HNO3 recovery
- b. Description of process

Fig: Acid recovery in Purex process

- 5.3.9 Waste disposal
 - a. Liquid waste
 - b. Gaseous waste
- 6.0 Thorex Process
 - 6.1 Introduction
 - 6.1.1 History
 - a. Evolution from "23" process through Interim-23 to Thorex
 - 6.1.2 Purpose and need of process
 - 6.1.3 Scope of process
 - 6.1.4 Specifications on final product
 - 6.1.5 Advantages and disadvantages of process
 - 6.1.6 Site employing process
 - 6.1.7 Present status
 - 6.2 Process Characteristics
 - 6.2.1 Use of nitrate acid-deficient system
 - 6.2.2 Characteristics of U as affecting Thorex

Table: Uranium separation factors

6.2.3 Characteristics of Th as affecting Thorex process

Table: Thorium separation factors

6.2.4 Characteristics of Pa as affecting Thorex

Table: Pa separation factors

6.2.5 Characteristics of fission products as affecting Thorex

Table: F. P. distribution between TBP-Amsco and

aqueous phases

6.2.6 Description of solvent and properties

Table: Physical properties of solvent

6.2.7 Description of feed materials and properties

Table: Physical properties of feed

6.3 Process Description

6.3.1 Flowsheet

Fig: Simplified flowsheet of Thorex process

6.3.2 Feed preparation

Table: Thorex dissolver offgas composition

6.3.3 Extraction

a. Description of extraction step

b. Extraction variables

Fig: Effect of temperature on extraction

c. Decontamination factor from Pa and FP's

d. Th and U losses

e. Column equilibrium diagrams

Fig: Column equilibrium diagram

6.3.4 Pa recovery

6.3.5 Partition

a. Description of partition step

b. Partition variables

Fig: Effect of temperature on partition

6.3.6 Thorium recovery

- a. Isotopic composition (Th²³², Th²³⁴, Pa²³³, and Th²²⁸) of stream
- b. Molar concentrations

c. Evaporation

d. Disposal of waste

6.3.7 Stripping

a. Description of stripping step

b. Stripping variables

Fig: Effect of temperature on stripping

6.3.8 Uranium recovery

a. Silica gel adsorption for Pa decontamination

b. Small ion exchange column

c. Large ion exchange column

d. Eluant composition and function

- e. Disposal of aqueous effluent
- f. Product composition
- g. Uranium losses

6.3.9 Solvent recovery

Fig: Solvent recovery flowsheet

- a. Na₂CO₂ wash
- b. Centrifugation
- c. Make-up solvent

6.3.10 Waste disposal

7.0 Miscellaneous Processes

Fig: Other Fuel Reprocessing Methods

- 7.1 Other Solvent Extraction Processes
 - 7.1.1 Pertinent remarks regarding origin, reasons for and history of processes
 - 7.1.2 Tabulation of processes showing purpose, solvent, development site and remarks about each
- 7.2 Other Precipitation Processes

- 7.2.1 Pertinent remarks regarding origin, reasons for and history of processes
- 7.2.2 Tabulation of processes showing purpose, reagents, development site and remarks about each
- 7.3 Volatility Processes
 - 7.3.1 Pertinent remarks regarding origin, reasons for and history of processes
 - 7.3.2 Tabulation of processes showing purpose, reagents, development site and remarks about each
- 7.4 Alloy Separation Processes
 - 7.4.1 Pertinent remarks regarding origin, reasons for and history of processes
 - 7.4.2 Tabulation of processes showing purpose, reagents, development site and pertinent remarks about each
- 7.5 Fyroprocesses
 - 7.5.1 Pertinent remarks regarding origin, reasons for and history of processes
 - 7.5.2 Tabulation of processes showing purpose, reagents, development site and pertinent remarks about each
- 7.6 Electrolytic Processes
 - 7.6.1 Pertinent remarks regarding origin, reasons for and history of processes
 - 7.6.2 Tabulation of processes showing purpose, reagents, development site and pertinent remarks about each
- 7.7 Adsorption Processes
 - 7.7.1 Pertinent remarks regarding origin, reasons for and history of processes
 - 7.7.2 Tabulation of processes showing purpose, reagents, development site and pertinent remarks about each

Outline for Chapter IV

CHEMICAL OPERATIONS

- 1.0 Introduction
- 2.0 Dissolution
- 3.0 Oxidation-Reduction
- 4.0 Electrolysis
- 5.0 Precipitation and Crystallization

1.0 Introduction

2.0 Dissolution

- 2.1 Introduction
- 2.2 Chemical Processes

2.2.1 Uranium-aluminum in HNO3

- a. Stoichiometry
- b. Thermodynamics
- c. Catalysis
- d. Rate data
- e. Fumeless dissolution
- f. Offgas treatment see "absorption," "adsorption," and "condensation"
- 2.2.2 Uranium-aluminum in NaOH
 - a. Stoichiometry
 - b. Thermodynamics
 - c. Rate data
 - d. Dejacketing applications
 - e. Solids removal

2.2.3 Thorium-aluminum in HNO3

- a. Stoichiometry
- b. Thermodynamics
- c. Catalysis
- d. Rate data

2.2.4 Uranium-zirconium in aqueous HF-HNO3

- a. Stoichiometry
- b. Thermodynamics
- c. Rate data

2.2.5 Uranium-zirconium by HF in fused salt

- a. Rate data
- b. Solubility
- c. Fission product behavior

2.2.6 Uranium-stainless steel in dilute aqua regia

- a. Stoichiometry
- b. Thermodynamics
- c. Rate data
- d. Acid recovery

2.2.7 Uranium-stainless steel in H2SO1

a. Chemical data

2.2.8 HRT-CP solids dissolving

- a. Stoichiometry
- b. Thermodynamics
- c. Rate data
- d. Magic concentration of H2SOL
- 2.2.9 ThO2 dissolution
 - a. Effect of firing temperature
 - b. Effect of radiation

2.3 Dissolution Equipment

Fig: Types of dissolution equipment

2.3.1 Batch vs. continuous

2.3.2 Flooded vs. trickle

2.3.3 Criticality

a. Slab dissolver

2.3.4 Methods of charging

a. Interlocks

b. Crash plates

2.3.5 Solids discharging dissolver

3.0 Oxidation-Reduction

3.1 Introduction

3.1.1 Oxidation potential

Fig: Oxidation potentials of heavy elements

3.2 Applications

3.2.1 Sodium dichromate

a. Redox feed

b. Redox IBP Pu stream

3.2.2 Sodium bismuthate - Pu⁺⁴ to Pu⁺⁶ after precipitation and redissolution in BiPO_L process

- 3.2.3 Fe⁺⁺ to take Pu⁺⁶ to Pu⁺³, followed by 1 <u>N</u> HNO₃ to take Pu⁺³ to Pu⁺⁴ BiPO₁ process
- 3.2.4 Ferrous sulfamate or ferrous ammonium sulfate and sulfamic acid Purex
- 3.2.5 H202 BiPOh, Redox
- 3.2.6 NaNO2 BiPO1, Redox

- 3.2.8 Hydrazine 25 process
- 3.2.9 HNO3
- 3.2.10 KMnOL Redox dissolver solution for Ru removal
- 3.2.11 White or ultraviolet light for reduction of Pu to +3 state -

4.0 Electrolysis

- 4.1 Introduction
 - 4.1.1 Thermodynamics
- 4.2 Applications
 - 4.2.1 Rala
 - 4.2.2 Equipment decontamination
 - 4.2.3 Excer
 - 4.2.4 Fused salt electrolysis for decontamination of uranium
 - 4.2.5 Electrolytic dissolution of stainless steel in HNO3
- 4.3 Calculations and Design Information
 - 4.3.1 Overvoltage
 - 4.3.2 Current efficiency
- 5.0 Precipitation and Crystallization
 - 5.1 Introduction
 - 5.1.1 Solubility
 - a. Retrograde solubility
 - 5.1.2 Precipitation carriers
 - 5.1.3 Nucleation and rate of crystal growth
 - 5.1.4 Energy effects
 - 5.1.5 Agitation and washing

5.2 Applications

5.2.1 BiPO process

a. Oxidation state of Pu

b. UNH concentration

c. Iron concentration

d. HNO3 concentration

e. Bismuth concentration

f. H PO concentration

g. Temperature

h. Rate of addition of reagent

i. Time of digestion

j. Order of addition of reagents

5.2.2 Rala

5.2.3 Thorium oxalate

a. Importance of rate of agitation

5.2.4 MnO, scavenging

5.2.5 Cs recovery - Hanford

5.3 Equipment Description

Fig: Precipitation equipment

5.3.1 BiPOL precipitators

5.3.2 RaLa - Stang reactor

5.3.3 Thorium oxalate jet precipitator

5.3.4 Dorr thickeners

5.3.5 Activated sludge

5.4 Calculations and Design Information

5.4.1 Calculation of yield

5.4.2 Solubility data or phase diagrams

Outline for Chapter V

MECHANICAL OPERATIONS

- 1.0 Introduction
- 2.0 Agitation
- 3.0 Centrifugation
- 4.0 Filtration (Liquid-Solid)
- 5.0 Filtration (Gas-Liquid and Gas-Solid)
- 6.0 Fluidization (Gas-Solid)
- 7.0 Physical Treatment

1.0 Introduction

1.1 Minimization of Maintenance

1.1.1 Simplicity

- 1.2 Minimization of Leakage
- 1.3 Equipment Duplication (double-valving, etc.)

2.0 Agitation

2.1 Introduction

2.1.1 Need and scope

2.1.2 Singular characterisitcs of radiochemical applications

- a. Leakage
- b. Splashing
- 2.2 Mechanically Driven Impeller

2.2.1 Theory

- a. Power per unit volume
- 2.2.2 Applications

- a. BiPO, precipitation tank
- b. BiPO, precipitate solution tank
- c. Feed adjustment tanks Thorex, SR, ICPP
- d. Mixer-settlers (q.v.)
- 2.2.3 Operational problems
 - a. Seals Fig.: Typical Seals on Agitator Shafts in Radiochemical Use
 - b. Lubrication Fig.: Lubrication of Agitator Bearings in Remote Maintenance Plant
- 2.2.4 Design considerations
 - a. Fower requirements
 - b. Tank geometry
 - c. Eaffles
- 2.3 External Recirculation
 - 2.3.1 Relative advantages
 - 2.3.2 Applications
 - a. Pump Hanford and ORNL Metal Recovery mining techniques
 - b. Steam jet BiPO, precipitation
 - 2.3.3 Operational problems
 - 2.3.4 Design considerations
 - a. Power requirements
 - b. Successful geometry
- 2.4 Gas Sparger (Air or Inert Gas)
 - 2.4.1 Description and limitations
 - 2.4.2 Applications
 - a. Air nearly all vessels, ICPP
 - b. Inert gas SIW dissolver, ICPP

2.4.3 Operational difficulties

- a. Gas disposal problem
- b. Entrainment problem
- 2.4.4 Design considerations
 - a. Volume gas required
 - b. Method of introducing gas
 - (1) Open end dip tube
 - (2) Perforated dip tube
 - (3) Perforated ring
 - (4) Sintered or sieve plate
- 2.5 Steam Sparging
 - 2.5.1 Applications
 - a. BiPO₄ dissolver, metal solution storage tanks, precipitator, precipitate catch tank, precipitate solution tank
 - 2.5.2 Operational problems
 - a. Heating problem
 - b. Dilution problem
 - 2.5.3 Design considerations

a. Same as 2.4.4

2.6 Magnetic Stirrer

- 2.6.1 Description and theory
- 2.6.2 Applications
 - a. KAPL slurry tank
 - b. Old RaLa process
- 2.6.3 Operational difficulties
- 2.6.4 Design considerations

- a. Impeller enclosure
- b. Magnet strength required

3.0 Centrifugation

- 3.1 Introduction
 - 3.1.1 Scope
 - 3.1.2 Singular characteristics of radiochemical applications
 - a. Heat generation
 - b. Value of product

3.2 Batch Basket Centrifuge

3.2.1 Description

Fig.: Centrifuge for BiPOh Process

3.2.2 Theory

3.2.3 Applications

- a. Solvent extraction feed clarification Hanford Metal Recovery, Hanford Redox, Hanford Purex (optional), SR
- b. Solvent clean-up Hanford Purex, Thorex (no longer used)
- c. BiPOh
- d. RaLa (Idaho)
- e. Pu recovery SR, Hanford
- f. MCFPPP
- 3.2.4 Operational problems
 - a. Splash, spray
 - b. Lubrication
 - c. Reslurrying
- 3.2.5 Design donsiderations

- a. Capacity
- b. Holdup
- c. Force required

3.3 Hydroclones

- 3.3.1 Description
- 3.3.2 Theory
- 3.3.2 Applications
 - a. HRT-CP
 - b. HRT loops
 - c. Solvent clean-up -Thorex

- Fig.: Hydroclone Nomenclature
- Fig.: Hydroclone for HRT-CP
- Fig.: Forces in Radial Flow Hydroclone
- Fig.: Forces in Axial Flow Hydroclone
- Fig.: Efficiency of Separation vs. Pressure Drop
- Fig.: Use of Multiple Clone Systems
- 3.3.4 Operational problems
 - a. Backmixing Fig.: Effect of Backmixing of Efficiency

flow Pot

- b. Underflow pot Fig.: Circulation in Hydroclone Under-
- 3.3.5 Design considerations
 - a. Geometry (underflow port, vortex finder, etc.)
 - b. Efficiency
 - c. Pressure drop

3.4 ----

- 3.4.1 Thoria slurry dewatering England
- 3.4.2 Fused salt-liquid metal systems England

4.0 Filtration (Liquid-Solid)

4.1 Introduction

4.1.1 Scope

4.1.2 Constant pressure vs. constant rate

4.1.3 Singular characteristics of radiochemical applications

- a. Difficulty of dressing remotely
- b. Need for high efficiency
- Small volume of solids, usually c.
- d. Cake handling
- e. Radiation damage
- 4.2 Sintered Metal or Glass
 - 4.2.1 Description

 - a. Star, cone, etc. Fig.: Typical Filters for Radiochemical Use
 - 4.2.2 Theory
 - a. Pore size
 - 4.2.3 Applications
 - a. Dissolver solutions
 - (1) MIR (star filter)
 - (2) ICPP, original installation
 - (3) Redox Pilot Plant ORNL
 - (4) Purex Pilot Plant ORNL
 - (5) "25" Pilot Plant ORNL
 - (6) "23" Pilot Plant ORNL
 - b. RaLa Idaho (metal)
 - c. RaLa ORNL (glass)
 - 4.2.4 Operational difficulties
 - a. Corrosion enlargement of pores
 - b. Plugging
 - 4.2.5 Design considerations

- a. Capacity
- b. Pressure drop through septum
- c. Wash water requirements
- d. Blower requirements for vacuum filtration
- 4.3 Wire Baskets
 - 4.3.1 Description, including size of opening
 - 4.3.2 Applications
 - a. Clean-up of solvent extraction feed ICPP (expanded)

4.4 Fiberglas

- 4.4.1 Description
- 4.4.2 Theory
- 4.4.3 Applications
 - a. Scrub streams Redox, Thorex
 - b. Solvent streams Thorex, SR
 - c. Solvent clean-up SR
 - d. Particulate removal from interfacial crud Thorex
- 4.4.4 Design considerations
 - a. Fiber density
 - b. Fiber diameters
 - c. Pressure drop
- 4.5 Rotary Drum Filter
 - 4.5.1 Conventional equipment
 - a. Relative ease of shielding for alpha radiation
 - 4.5.2 Applications
 - a. ThO, preparation ORNL
 - b. KAPL wastes
 - 4.5.3 Design considerations

a. Alpha containment

b. Compare 4.2.5

- 4.6 Magnetic Filter
 - 4.6.1 Description

Fig.: Photograph of Installed Magnetic Filter

- a. Electromagnet
- b. Powder
- c. Support bars
- d. Filter aid
- 4.6.2 Theory

Fig.: Gauss vs. Pipe Diameter

- a. Magnet strength
- b. Comparison with conventional septum
- 4.6.3 Applications
 - a. UNOP tests, 3" diameter
- 4.6.4 Operational problems
 - a. Establishment of bed
 - b. Recovery of powder
 - c. Corrosion of powder
- 4.6.5 Design considerations
 - a. Pressure drop
 - b. Rupture strength
 - c. Weight limitations
 - d. Shaping of pole pieces
- 4.7 Edge Filter (Cuno)
 - 4.7.1 Description Fig.: Edge Filter
 - 4.7.2 Applications

5.0 Filtration (Gas-Liquid and Gas-Solid)

- 5.1 Introduction
 - 5.1.1 Importance (biological)
 - 5.1.2 Efficiency required
 - 5.1.3 Mechanisms
- 5.2 AEC Paper
 - 5.2.1 Scope
 - a. Particle size for which effective
 - b. Particle concentration for which suitable
 - c. Capacity
 - d. Other limitations
 - 5.2.2 Applications
 - a. Calciner off gas SR
 - b. Waste incinerator off gas ANL
 - c. Etc. (widely used)
 - 5.2.3 Filter replacement methods
- 5.3 Bag Filters
- 5.3.1 Scope
 - a. Particle size
 - b. Particle concentration
 - c. Capacity
 - d. Other limitations
 - 5.3.2 Applications
 - a. Calciner off gas SR, Hanford
 - 5.3.3 Bag changing technique

5.4 Sand Filters

5.4.1 Scope

a. Particle size

b. Particle concentrations

c. Capacity

d. Pressure drop

5.4.2 Applications

a. Hot off gas - SR, Hanford

5.5 Fiberglas Filters

5.5.1 Scope

a. Particle size

b. Particle concentration

c. Capacity

5.5.2 Applications

a. Process off gas lines

b. Service lines

5.5.3 Design considerations

a. Fiber size

b. Packing density

5.6 Electrostatic Precipitators

5.6.1 Scope

a. Particle size

b. Efficiency

5.6.2 Applications

5.6.3 Design

- a. Voltage required
 - b. Geometry
- 5.6.4 Operational difficulties

6.0 Fluidization (Gas-Solid)

- 6.1 Introduction
 - 6.1.1 Characteristic features of radiochemical applications
- 6.2 Theoretical Background
 - 6.2.1 Types of fluidized beds
 - 6.2.2 Particle size and size range
 - 6.2.3 Pressure drop
 - 6.2.4 Entrainment
 - 6.2.5 Heat transfer

6.3 Applications

6.3.1 $UF_{4} \longrightarrow UF_{6}$ (England) 6.3.2 $UNH \longrightarrow UO_{3}$ (see Calcination) 6.3.3 $ANN \longrightarrow Al_{2}O_{3}$ (see Calcination) 6.3.4 UF_{4} dehydration - UNOP

7.0 Physical Treatment

- 7.1 Introduction
- 7.2 Materials Handling

7.2.1 Slug charging Fig.: Slug Charging Mechanism

- a. Universal loader UNOP
- 7.2.2 Solids discharging dissolver UNOP

Fig.: Continuous Solids Discharging Dissolver 7.2.3 Fission product separation, special equipment for

- 7.3 Physical Separations
 - 7.3.1 Sawing
 - 7.3.2 Grinding
 - 7.3.3 Dejacketing Fig.: Operation of Dejacketing Devices
 - a. Banana peeler
 - b. Unwinder
 - c. Derodder
- Fig.: McIntosh-Hemphill Derodder

7.3.4 Chopping

Outline for Chapter VI

FLUID FLOW

- 1.0 Introduction
- 2.0 Piping and Pipe Connections
- 3.0 Pumps
- 4.0 Valves
- 1.0 Introduction
- 2.0 Piping and Pipe Connections
 - 2.1 Introduction
 - 2.1.1 Importance of integrity
 - 2.1.2 Need of connections for maintenance reasons
 - a. Relation to type of maintenance
 - 2.1.3 Tubing vs. pipe
 - 2.1.4 Thermal expansion
 - 2.1.5 Head losses calculated by conventional means
 - 2.2 Welded Joints
 - 2.2.1 Specifications
 - 2.2.2 Welder qualification
 - 2.2.3 Inspection
 - 2.2.4 Screwed connections, back-welded
 - 2.3 Flanged Joints

2.3.1 Gasket types and materials

Fig: Gaskets suitable for radiochemical use

2.3.2 Gasket measurement - HRT-CP

Fig: Device for accurate gasket measurement

a. Belleville springs

Fig: Belleville springs

- b. Ferrules and counterbore
- c. Other

2.3.4 Leak detection - HRT-CP

- 2.4 Tubing Fittings
 - 2.4.1 Types
 - a. Flared
 - b. Compression
 - 2.4.2 Tendency to weep
- 2.5 Quick Disconnects
 - 2.5.1 Types
 - a. RaLa design
 - b. Graylok
 - c. Nicholson-Irvine design

Fig: Quick disconnects for underwater maintenance

d. Other

2.5.2 Applications

- a. Decontamination lines Thorex
- b. Service lines ICPP (jets, spargers, jackets not normally

used)

c. Instrument lines - MCFPPP

2.6 High Pressure Fittings

2.6.1 Description

2.6.2 Applications

a. HRT-CP

- b. Centrifuge plow hydraulic controls
- c. Centrifuge sluicing sprays
- 2.7 Remote Disconnects See Chapter II
- 3.0 Pumps
 - 3.1 Introduction
 - 3.1.1 Characteristics
 - a. Capacity
 - b. Head
 - c. Power
 - d. Efficiency
 - e. Reliability

3.1.2 Special seals

Fig: Seals for pumps in radiochemical applications

- a. Leakage specifications
- 3.2 Turbine Pumps
 - 3.2.1 Distinguishing characteristics in radiochemical applications
 - 3.2.2 Types
 - a. Deep well Hanford

Fig: Deep well turbine pump

b. Regenerative - Redox

Fig: Regenerative turbine pump

- 3.2.3 Operational difficulties
- 3.2.4 Design

3.3 Piston Pumps

- 3.3.1 Distinguishing characteristics
- 3.3.2 Applications

- a. Metering cold streams
- b. ---- KAPL

3.3.3 Operational difficulties

- 3.3.4 Design
- 3.4 Gear Pumps

3.4.1 Distinguishing characteristics

3.4.2 Applications

3.5 Centrifugal Pumps

3.5.1 Characteristics distinguishing them in radiochemical applications

- 3.5.2 Applications
- 3.6 Canned Rotor Pumps
 - 3.6.1 Distinguishing characteristics

Fig: Canned rotor pump developed for radiochemical

use

3.6.2 Applications

- a. HRT-CP
- b. BrF3 BNL
- c. Solvent recovery ICPP, Hanford, Thorex
- d. Metal recovery (ORNL)

3.6.3 Operational difficulties

- a. Alignment
- b. Bearing lubrication
- 3.6.4 Design considerations
- 3.7 Hytor
 - 3.7.1 Distinguishing characteristics
 - 3.7.2 Applications

- a. Offgas vacuum
- b. Filter vacuum
- 3.7.3 Design considerations
- 3.8 Diaphragm Pumps

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3.8.1 Characteristics of applications which distinguish them from conventional

Fig: Remote head diaphragm pump

3.8.2 Applications

- a. Solvent extraction feed ICPP, ORNL
- b. HRT solids injection
- 3.8.3 Operational problems
- 3.8.4 Design considerations
- 3.9 Progressing Cavity Pumps (Moyno)

3.9.1 Distinguishing characteristics

3.9.2 Applications

- a. Waste sampling ICPP
- b. Slurries
- c. Highly concentrated UNH solutions
- 3.9.3 Operational problems
- 3.9.4 Design considerations

3.10 Peristaltic Pumps

3.10.1 Distinguishing characteristics

Fig: Two types of Peristaltic pump

3.10.2 Applications

- a. Development work
- b. Early times

- 3.10.3 Operational difficulties
- 3.10.4 Design considerations
- 3.11 Steam Jets
 - 3.11.1 Characteristics which distinguish them for radiochemical applications

3.11.2 Applications

- a. Hot feed SR
- b. Waste evaporator feed ICPP, SR
- c. Sampling BiPO₄, "25" pilot plant (ORNL), Redox pilot plant (ORNL)
- d. Internal recirculation of decontaminating solutions ICPP, Thorex
- e. Metering solvent ORNL Metal Recovery
- f. Metering feed ORNL Metal Recovery
- g. Elevating feeds ORNL Metal Recovery
- h. Offgas vacuum ORNL Filot Flant
- .3.11.3 Operational difficulties
 - a. Dilution
 - b. Temperature increase
 - c. Vapor lock
 - 3.11.4 Design considerations

3.12 Air Jets

- 3.12.1 Distinguishing characteristics
- 3.12.2 Applications
 - a. Sampling
- 3.12.3 Design considerations

- 3.13 Displacement Pumping
 - 3.13.1 Distinguishing characteristics
 - 3.13.2 Types
 - a. Displacement gas (blow case)
 - (1) Final product transfer, ICPP
 - (2) Molten salt transfer Volatility Pilot Plant
 - b. Displacement liquid: methylcyclohexane hot feed, "25" pilot plant
 - c. Displacement solid lowering tank into tank (France)
 - 3.13.3 Operational problems
 - a. Control difficulty (gas)
 - 3.13.4 Design considerations

3.15 Airlifts

- 3.15.1 Distinguishing characteristics
 - a. No moving parts
- 3.15.2 Applications
 - a. Hot feed metering ICPP (expanded), Thorex
- 3.15.3 Operational difficulties
 - a. Entrainment in off-gas
 - b. Plugging in concentrated solutions
- 3.15.4 Design considerations
- 3.16 Vapor Transfer (Temperature Differential)
 - 3.16.1 Description
 - 3.16.2 Applications
 - a. UF6 transfer ORNL-VPP, ANL
 - 3.16.3 Design considerations

- 3.17 Egyptian Water Wheel
 - 3.17.1 Description
 - 3.17.2 Applications
 - a. EBR blanket processing plant feed

4.0 Valves

- 4.1 Introduction
 - 4.1.1 Characteristics of applications which distinguish them from conventional applications
 - 4.1.2 Types of applications
 - a. Flow control
 - b. Flow interruption
 - c. Check valves
 - (1) Pulse column use
 - (2) Other uses
 - d. Safety valves and frangible disks
 - e. Instrument valves

4.2 Mechanical Valves

- 4.2.1 Special features for radiochemical use
 - a. Operator
 - (1) Bellows
 - (2) Diaphragm
 - (3) Extension handles
 - (4) Motor
 - (5) Solenoid Redox pilot plant sampling valve

b. Seal

- (1) Bellows
- (2) Packed
- (3) Diaphragm
- c. Seat
 - (1) Teflon developed at ORNL
 - (2) Stellite stem, S. S. seat ICPP
 - (3) Stellite seat, S. S. plug HRT
 - (4) Hastelloy seat, Carpenter 20 plug HRT
 - (5) Etc.

4.3 Freeze Valves

- 4.3.1 Characteristics which distinguish them for radiochemical use
- 4.3.2 Applications
 - a. HRT-CP

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- Fig: Freeze valve in aqueous line
- b. Molten salt Volatility Pilot Plant

Fig: Freeze valve in molten salt line

c. Thorex

4.3.3 Operational difficulties

4.3.4 Design considerations

4.4 Air Block Valve (Irvine)

4.4.1 Description

Fig: Irvine air block valve

4.4.2 Application

a. Recycle process system - Thorex

Outline for Chapter VII HEAT TRANSFER OPERATIONS

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- 1.0 Introduction
- 2.0 Heat Transfer Without Change of Phase
- 3.0 Boiling and Evaporation
- 4.0 Vapor Condensation
- 5.0 Calcination

1.0 Introduction

- 1.1 Mechanisms
- 1.2 Governing Philosophy
 - 1.2.1 Avoid contamination of cooling or heating medium
 - a. Recirculation of medium
 - 1.2.2 Avoid introduction of medium into process stream
 - 1.2.3 Ease of equipment decontamination
- 2.0 Heat Transfer Without Change of Phase
 - 2.1 Introduction
 - 2.2 Jacketed Vessels
 - 2.2.1 Advantages in Radiochemical Plant

2.2.2 Applications

- a. Dissolvers BiPOL, ICPP, ORNL pilot plant, HRT-CP
- b. BiPO, metal solution storage tanks
- c. Feed make-up tanks
- d. Decay storage tanks HRT-CP
- 2.2.3 Operational problems

2.2.4 Design

- a. Heat transfer coefficients
- 2.3 Coils Inside Vessels

2.3.1 Advantages

2.3.2 Applications

a. BiPO dissolvers, etc.

b. Sr, extensively

c. Dissolver - RaLa

2.3.3 Operational difficulties

a. Leaks

b. Decontamination

2.3.4 Design

a. Heat transfer coefficients

2.4 Coils Wrapped Around Vessels

2.4.1 Advantages in radiochemical plant

2.4.2 Applications

a. ANL volatility

2.4.3 Design calculations

a. Area determination

b. Heat transfer coefficients

2.5 Shell-and-Tube Heat Exchangers

2.5.1 Applications

a. Liquid nitrogen cooling of offgas charcoal beds

2.5.2 Operational problems

2.5.3 Design

2.6 Steam Spargers

2.6.1 Advantages in radiochemical plant

2.6.2 Applications and disadvantages

- a. BiPO, dissolver
- b. ICPP (optional)
- c. Other
- 2.6.3 Operating problems
- 2.6.4 Design considerations
- 2.7 Electric Resistance Elements
 - 2.7.1 Advantages and disadvantages in radiochemical plant
 - a. High heat flux obtainable
 - b. Ease of control
 - c. Tendency to burn out

2.7.2 Applications

- a. Furnaces ORNL-VPP
- b. Strip heaters ORNL-VPP, HRT-CP
- c. Finned strip heaters in offgas BiPOh, Redox
- d. Resistance cable UF6 transfer lines
- e. Immersion heaters

2.7.3 Design considerations

- a. Maximum permissible surface temperature
- b. Spacing to provide uniform heat distribution

2.7.4 Special techniques

- a. Casting Inconel-tubing heaters in high copper alloy or aluminum
- 2.8 Electric Autoresistance Heating
 - . . 2.8.1 Description and advantages

Fig: Autoresistance heating installation

2.8.2 Applications

a. ORNL-VPP

2.8.3 Operational problems

a. Impedance balancing

b. Stray currents

c. Input terminal

Fig: Temperature control at input terminal

2.8.4 Design considerations

a. Current requirements

Fig: Temperature distribution at pipe junctions

b. Heat losses at fittings or terminals

c. Insulation uniformity

2.9 Induction Heating

2.9.1 Description and advantages

2.9.2 Applications

a. Oxide slagging

b. Zone melting

2.9.3 Operational problems

a. Size of power supply

2.9.4 Design considerations

2.10 Pump Energy

2.10.1 Use for HRT loops

3.0 Boiling and Evaporation

3.1 Introduction

3.1.1 Theoretical background

3.1.2 Vapor recompression - BNL waste

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- 3.1.3 Control considerations
- 3.2 Steam-Jacketed Pot
 - 3.2.1 Application
 - a. Intercycle evaporator = "25" process
 - 3.2.2 Operational problems
 - 3.2.3 Design
 - a. Heat transfer coefficients
- 3.3 Conventional Shell-and-Tube Boiler
 - 3.3.1 Applications
 - a. Hanford waste
 - 3.3.2 Operational difficulties
 - 3.3.3 Special techniques
 - a. Joining tubes to tube sheets
 - 3.3.4 Design
- 3.4 Vertical Tube, Gravity Recirculation
 - 3.4.1 Advantages for radiochemical use
 - 3.4.2 Applications
 - a. Purex Hanford
 - b. "25" process ICPP
 - 3.4.3 Operational problems
 - 3.4.4 Design
- 3.5 Bayonet Tube Bundles
 - 3.5.1 Advantages in radiochemical plant
 - 3.5.2 Applications
 - a. Hexone recovery still ICPP
 - b. Purex, Redox Hanford
 - 3.5.3 Operational problems

Fig: Bayonet tube bundle for remote maintenance

plant

3.5.4 Design

3.6 Internal Coils in Pot

3.6.1 Advantages in radiochemical plant

3.6.2 Applications

a. Redox ICU

b. SR

3.6.3 Operational problems

a. SR burnout

3.6.4 Design calculations

3.7 Falling Film Evaporator

3.7.1 Applications

a. "25" pilot plant - intercycle evaporator

3.7.2 Operational problems

a. Control

3.7.3 Design

3.8 Glycerine Bath

3.8.1 Applications

a. BiPO, product concentration

3.8.2 Difficulties

3.9 Flash Evaporation Development - SR

4.0 Vapor Condensation

4.1 Introduction

4.1.1 Theoretical background

4.1.2 Updraft vs. downdraft

4.1.3 Effect of large quantities of inerts

4.1.4 Snow or fog formation

Fig: Conditions for fog formation in condensers

4.2 Conventional Shell and Tube

4.2.1 Applications - ICPP, Hanford, ORNL

4.2.2 Operational problems ?

4.2.3 Design - conventional

4.3 Shell and Finned Tube, Vapor Outside Tube, Falling Film

4.3.1 Description

4.3.2 Applications

a. Redox

b. Purex - Hanford

4.3.3 Design considerations

4.4. Jacketed Pipe

4.4.1 Applications

a. Coolers - expanded ICPP, Thorex

4.4.2 Design = conventional

4.5 Coil Within Vessel, Vapor Outside Coil

4.5.1 Advantages in radiochemical plant

4.5.2 Applications

a. Sr, almost universally

b. Dissolver offgas - BiPO

4.5.3 Operational problems

4.5.4 Design

a. Area determination

b. Outside film coefficient

- c. Overall coefficient
- d. Coil radius; spacing
- 4.6 Coil Within Vessel, Vapor Inside Coil

4.6.1 Applications

a. Offgas cold traps (liquid nitrogen coolant)

4.6.2 Design

a. Capacity

b. Fabrication techniques

4.7 Coils Wrapped Around Vessel; Spray Metal Bonded

4.7.1 Description and advantages in radiochemical plant

Fig: Bonding of cooling coils to condenser shell

4.7.2 Applications

a. ANL volatility

4.7.3 Design

a. Coil area requirement

b. Calculation of mean path through metal

Fig: Determination of mean heat path

c. Overall coefficients

- (1) Water in coil
- (2) Air in coil

4.8 Contact Condenser

4.8.1 Advantages and limitations in radiochemical plant

4.8.2 Applications

a. Hanford low level activity

4.8.3 Design - conventional

4.9 Egg-Crate Baffled Cold Traps

. . 4.9.1 Description and advantages

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Fig: Extended surface for UF6 cold trap
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4.9.2 Applications

a. ORNI-VPP

4.9.3 Design

a. Capacity

b. Baffle spacing Fig: Calculation of baffle spacing

c. Thermal stresses

4.10 Fluidized Cold Trap

4.10.1 Description

Fig: Continuous cold trap

4.10.2 Advantages

a. Continuous

4.10.3 Possible applications

a. UF₆ - volatility

4.10.4 Design

a. Capacity

b. Heat transfer coefficients

c. Stripping section

d. Entrainment collection

5.0 Calcination

- 5.1 Introduction
- 5.2 Stirred Pot Calciner

5.2.1 Description

a. Nature of product

5.2.2 Applications

a. UNH --- UO3

5.2.3 Operational problems

5.2.4 Design

a. Power requirement

b. Heat transfer

5.3 Screw Calciner

5.3.1 Description

Fig: Continuous screw calciner

a. Nature of product

5.3.2 Applications

a. UNH ---> UO3

5.3.3 Operational problems

5.3.4 Design

a. Power requirements

b. Heat transfer

5.4 Fluidized Bed Calciner

5.4.1 Description

a. Nature of product

5.4.2 Applications

a. UNH ---> UO3

b. Aluminum nitrate ---> Al203

5.4.3 Design

a. Fluidizing velocity

b. Heat transfer

5.5 Moving Bed

5.5.1 Description

5.5.2 Applications

a. UNH ---> UO3

- 5.6 Furnace
 - 5.6.1 Description
 - 5.6.2 Applications
 - a. Thorium oxalate ---> ThO2 ORNL

5.6.3 Design

- a. Heat requirements
- b. Temperature and time of firing

5.7 Flame calciner ?

Outline for Chapter VIII

SOLVENT EXTRACTION

- 1.0 Introduction
- 2.0 Mixer-Settlers
- 3.0 Pulse Columns
- 4.0 Other Extraction Equipment
- 5.0 De-Emulsification

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- 1.0 Introduction
 - 1.1 Theory
 - 1.1.1 Distribution
 - 1.1.2 Equilibrium data
 - 1.1.3 Column functions
 - a. Extraction
 - b. Scrubbing
 - c. Stripping
 - 1.1.4 Calculation methods
 - 1.2 Equipment Characteristics
 - 1.2.1 Throughput
 - 1.2.2 Flooding
 - 1.2.3 Stage efficiency
- 2.0 Mixer-Settlers
 - 2.1 Introduction
 - 2.2 Agitation

2.2.1	Mechanical stirring		Fig.:	Mechanically Stirred Mixer- Settler
	а.	KAPL	14214	
	ъ.	SR		
2.2.2	2.2 Pump-mix			
	8.	KAPL	Fig.:	KAPL Pump-Mix Mixer-Settler
	ъ.	SR	Fig.:	Savannah River Pump-Mix Mixer-Settler
	c.	Whatley	Fig.:	Whatley Mixer-Settler
2.2.3	2.3 Airlift			
	a.	Chalk River	Fig.:	Airlift Mixer-Settler
	Ъ.	Harwell		
2.2.4	Pulsed			
	а.	Hanford		

- 2.2.5 Ultrasonic
- 2.2.6 Shrouded paddle

a. SR

- 2.3 Design Considerations
 - 2.3.1 Interfacial area

a. ANL (Rodger)

Fig.: Interfacial Area of Dispersed Phase

- 2.3.2 Stage efficiency
- 2.3.3 Density differences
- 2.3.4 Emulsion tendencies
- 2.3.5 Interface control

- 3.0 Pulse Columns
 - 3.1 Introduction

3.1.1 Advantages

Fig.: Pulse Column

3.2 Applications

3.2.1 Purex - Hanford

3.2.2 Metal Recovery - Hanford, ORNL

3.2.3 "25" Process - ICPP

3.2.4 Thorex - ORNL

3.2.5 Other

a. Mallinkrodt

b. Fernald

3.3 Characteristic Features

3.3.1 Interface control

a. Dip lines

b. Capacitance probes

c. Floats

3.3.2 Backmixing

3.3.3 Emulsions and third phase

3.3.4 Interface crud

3.3.5 Pulsers

Fig.: Pulsing Mechanisms

a. Piston

b. Bellows

c. Steam

3.3.6 Flooding

a. Frequency - amplitude product, effect on

b. Relative flow rates, effect on

c. Extraction height, effect on

- 3.3.7 Determination of flooding
 - a. McNamee method Fig.: Analytical Determination of Flooding
- 3.3.8 Determination of stage height
- 3.3.9 Pulse effects
 - a. Frequency amplitude product
 - b. Wave form
 - c. Amplitude
- 3.3.10 Plate geometry
 - a. Spacing
 - b. Thickness
 - c. Size of perforations
 - d. Spacing of perforations
 - e. Number of perforations

3.3.11 Concatenation Fig.: Diagram of Concatenated Pulse Column

- a. Aqueous and organic check valves
- 3.3.12 Special plate design Fig.: Special Pulse Column Plates
 - a. Zebra plates
 - b. Nozzle plates
 - c. Louver plates
- 4.0 Other Extraction Equipment
 - 4.1 Packed Columns Redox, ICPP
 - 4.2 Spray Columns LMFR Extraction
 - 4.3 Rushton

Fig: Rushton Solvent Extraction Contactor 4.4 Scheibel - ORGDP, U recovery from cleaning solution

- Fig: Scheibel Contactor for Uranium Recovery
- 4.5 Pump-clone UNOP
- Fig: Diagram of Minimal-Contact-Time Contactor

4.6 York

4.7 Cannon

5.0 De-Emulsification

- 5.1 Introduction
 - 5.1.1 Characteristics of emulsions
 - 5.1.2 Theories of emulsion breaking
- 5.2 Equipment

5.2.1 Selas separator

- a. Thorex crud removal
- 5.2.2 Ultrasonic

5.2.3 Fiberglas - SR

- 5.3 Interface Jetting
- 5.4 Design Information
 - 5.4.1 Flow capacity
 - 5.4.2 Efficiency

Outline for Chapter IX

OTHER MASS DIFFUSION OPERATIONS

- 1.0 Introduction
- 2.0 Gas-Liquid Absorption
- 3.0 Adsorption
- 4.0 Drying
- 5.0 Ion Exchange
- 6.0 Distillation and Rectification
- 7.0 Steam Stripping
- 1.0 Introduction
 - 1.1 Equilibrium
 - 1.2 Ideal Stages

1.2.1 Material balance

1.2.2 Operating lines

- 1.3 Calculation of Number of Ideal Stages
- 1.4 Calculation of Number of Transfer Units
- 1.5 The Rate Equation
 - 1.5.1 Film theory
 - 1.5.2 Fugacity differences
 - 1.5.3 Diffusion

2.0 Gas-Liquid Absorption

- 2.1 Introduction
 - 2.1.1 Theoretical background
 - a. Henry's law
 - b. Absorption coefficients

2.1.2 Gas holders

2.1.3 0, addition techniques

2.2 Wetted Wall Towers (down draft condensers)

2.2.1 Description

2.2.2 Use for removal of nitrogen oxides from dissolver offgas

2.2.3 Design

a. Gas rate; liquid rate; L/V

b. HTU

c. Pressure drop negligible

2.3 Packed Towers (Raschig ring packing)

2.3.1 Theory

2.3.2 Applications

a. Offgas de-entrainment - BiPO, dissolvers

b. Fluorine disposal - K-25, Paducah

2.3.3 Design

a. Capacity

b. Gas and liquid rates; L/V

c. Pressure drop

d. Flow distributors

2.4 Bubble Cap Columns

2.4.1 Theory

2.4.2 Use for HNO3 recovery - SR, Hanford Purex

2.4.3 Operational problems ?

2.4.4 Design

a. H. E. T. S.

b. Liquid and gas rates; L/V

c. Pressure drop

- 2.5.1 Theory
- 2.5.2 Application to hot vessel offgas Thorex
- 2.5.3 Operational difficulties ?

2.5.4 Design

- a. H. E. T. S.
- b. Liquid and gas rates; L/V
- c. Pressure drop

2.6 Spray Towers

- 2.6.1 Theory
- 2.6.2 Applications
 - a. Fluorine disposal ORNL-VPP
 - b. Interhalogen disposal ANL-VPP
 - c. Dissolver offgas ICPP
- 2.6.3 Operational difficulties
 - a. Entrainment
 - b. Corrosion

2.6.4 Design

- a. Capacity
- b. Gas and liquid rates; L/V
- c. Pressure drop
- d. Spray pattern

3.0 Adsorption

- 3.1 Adsorption
 - 3.1.1 Theoretical background

- a. Equilibrium data
 - b. Heat of adsorption
- 3.1.2 Effect of regeneration
- 3.1.3 Effect of fission product heat generation
- 3.2 Charcoal Beds
 - 3.2.1 Equilibrium capacity
 - 3.2.2 Applications
 - a. Kr and Xe removal
 - b. I removal
 - 3.2.3 Desorption
 - a. Time required
- 3.3 Silica Gel Beds
 - 3.3.1 Equilibrium capacity
 - 3.3.2 Applications
 - a. Zr-Nb from process wastes KAPL
 - b. U-233 decontamination from Pa, Zr, No Thorex
 - 3.3.3 Desorption
- 3.4 Alumina
 - 3.4.1 Capacity
 - 3.4.2 Applications
 - a. Offgas drying before low-temperature beds ICPP
 - b. Water removal from freon refrigerant HRT-CP
 - c. Instrument air drying (commercial units)
- 3.5 NaF Beds
 - 3.5.1 Capacity
 - a. HF
 - b. UF6

Fig: UF6 equilibrium with NaF at various

temperatures

c. Fission product fluorides

3.5.2 Applications

- a. HF removal from F2 VPP
- b. Fission product removal from process stream VPP

c. UF6 safety traps

Fig: Concentration profile in UF6 safety trap

3.5.3 Operational difficulties

- a. Fines entrainment
- b. UF5 formation
- c. Heat transfer difficulties
- 3.5.4 Desorption
 - a. UF6 losses
 - b. Ability to re-use
- 3.6 AgNO3 Coated Packing for I2 Removal
 - 3.6.1 Description
 - 3.6.2 Capacity
 - 3.6.3 Regeneration

4.0 Drying

4.1 Introduction

4.1.1 Theoretical background

4.2 UF

4.2.1 Crystal structure - 2.5 hydrate vs. 0.75 hydrate

Fig: Photomicrograph of UF4 hydrates

4.2.2 Tray drying

4.2.3 Fluidized bed

4.3 RaLa Product

4.3.1 Infra-red plus aspiration

4.4 Gas Streams

4.4.1 Cold traps (see "condensation")

4.4.2 Desiccants (see "adsorption")

5.0 Ion Exchange

- 5.1 Introduction
 - 5.1.1 Theoretical background
 - 5.1.2 Cation resins
 - 5.1.3 Anion resins
 - 5.1.4 Radiation damage to resins

Table: Damage to selected resins exposed to radiation

Tauratio

5.1.5 Resin attrition

Fig: Attrition of Dowex-50 after 1000 hours circulation

- 5.1.6 Semipermeable membranes
- 5.2 Fixed Bed Exchangers
 - 5.2.1 Upflow vs. downflow

5.2.2 Applications

a. Pu isolation - SR, Purex Pilot Plant, ORNL Metal Recovery

- b. Rala
- c. U-233 recovery Thorex
- d. waste disposal

- e. Canal water cleanup
- f. Fractionation of radioisotopes
- 5.2.3 Design
 - a. Capacity
 - b. Regeneration

5.3 Higgins Contactor

.

Fig: Diagram of Higgins contactor

5.3.1 Description

- a. Pulsing mechanism
 - Fig: Resin pulsing schemes
- b. Slip-water ratio
- c. Resin valves

5.3.2 Applications

- a. Pu concentration Hanford
- b. Decladding stainless steel with H2SOL
- c. Excer ?
- d. Scrap recovery ?
- e. 36-in. column

5.3.3 Design considerations

- a. Capacity loading and stripping sections
- b. Pulse volume
- 5.4 Continuous Ion Exchange Equipment

5.4.1 Hydraulic ram

6.0 Distillation and Rectification

- 6.1 Introduction
 - 6.1.1 Theoretical background

b. Theoretical stages and transfer units

c. Rectification and reflux

6.2 Batch Retorts

6.2.1 High-temperature metal separation

Fig: Equipment for distillation of Magnesium metal

6.2.2 Solvent recovery - Redox Pilot Plant, "25" Pilot Plant

6.3 Packed Columns

6.3.1 Advantages

6.3.2 Applications

a. Raschig rings for UF6 - ORGDP

- b. Cannon packing for UF6 ORGDP, ANL Volatility
- c. Other BNL Volatility (helices)

6.3.3 Design Considerations

- a. Boil-up rate
- b. Flooding
- c. Holdup
- d. Throughput
- e. Reflux splitters

6.4 Bubble Cap Columns

6.4.1 Advantages

6.4.2 Applications

a. Darex all-glass column

6.4.3 Design

- · a. Conventional

- 6.5 Steam Distillation
 - 6.5.1 Theory
 - 6.5.2 Applications
 - a. Hexone recovery Hanford
 - b. TBP removal see "steam stripping"
 - 6.5.3 Design
 - a. Conventional
- 7.0 Steam Stripping
 - 7.1 Introduction
 - 7.1.1 Theoretical background
 - 7.2 Equipment
 - 7.2.1 Packed columns
 - 7.2.2 Bubble-cap columns
 - a. "25" process
 - b. Hanford Purex (intercycle)
 - 7.2.3 Sieve plate columns
 - a. "25" process
 - 7.2.4 ?
 - a. Hanford Redox ICU
 - b. Hanford Redox 3B effluent
 - c. Hanford Redox condensate stripper

Outline for Chapter X

INSTRUMENTATION

- 1.0 Introduction
- 2.0 General Design Considerations
- 3.0 Chemical Analysis by Means of Physical Properties
- 4.0 Temperature
- 5.0 Pressure
- 6.0 Flow
- 7.0 Radiation
- 8.0 Mass
- 9.0 Level
- 10.0 Noise
- 11.0 Specific Gravity
- 12.0 Control and Read-Out Instruments

1.0 Introduction

- 1.1 Physical Measurements
- 1.2 Chemical Measurements
- 1.3 Remote Operation
- 1.4 Problems Introduced by Radiation
 - 1.4.1 Materials of construction

1.4.2 Unit shielding

1.5 Typical Process Instrumentation Circuit

Fig: Typical Process Instrumentation Chart

- 2.0 General Design Considerations
 - 2.1 No Direct or Potentially Direct Connections Between Process and Operating Areas

- 2.2 Inaccessibleness of In-Cell Instruments During Operation
- 2.3 Duplication of Certain Components
- 2.4 Leak-Tight Systems
- 2.5 In-Cell and Out-Of-Cell Applications
- 2.6 Precision and Accuracy
- 2.7 Fneumatic and Electric Applications
- 2.8 Nature of Process Stream
- 2.9 Disposition of Signal
- 2.10 Type of Maintenance (Direct, Remote, Underwater)
- 3.0 Chemical Analysis by Means of Physical Properties
 - 3.1 Boiling Point
 - 3.2 Thermal Conductivity
 - 3.3 Mass Spectrograph
 - 3.4 pH
 - 3.5 Light Absorption
 - 3.6 Electrical Conductivity
- 4.0 Temperature
 - 4.1 Thermocouples
 - 4.2 Gas Bulbs
 - 4.3 Resistance Thermometers

5.0 Pressure

- 5.1 Bourdon Tube
- 5.2 Manometer
- 5.3 Strain Gage

6.0 Flow

6.1 Orifices

6.2 Rotometers

6.3 Vane Anemometer

6.4 Change in Sight Glass Level

6.5 Metering Pumps with "Flow Checkers"

6.6 Magnetic Flow Meter

6.7 Thermal Flow Meter

6.8 Air Lift Pump Meter

7.0 Radiation

- 7.1 Process Stream Measurements
- 7.2 In-Cell Atmosphere Measurements
- 7.3 Operating Area Measurements

8.0 Mass

- 8.1 Scales
- 8.2 Strain Gages
- 8.3 Null Balance

9.0 Level

.

- 9.1 Gamma Transmission
- 9.2 Dip Leg
- 9.3 Thermal Level Probe

Fig: Thermal Level Probe

9.4 Sonic

10.0 Noise

10.1 Microphone

11.0 Specific Gravity

11.1 Dip Leg

12.0 Control and Read-Out Instruments

Outline for Chapter XI AUXILIARY EQUIPMENT

- 1.0 Introduction
- 2.0 Carriers
- 3.0 Viewing Devices
- 4.0 Manipulators
- 5.0 Samplers
- 1.0 Introduction
- 2.0 Carriers
 - 2.1 Introduction
 - 2.1.1 I. C. C. regulations on radiation
 - 2.1.2 Weight limitations
 - 2.1.3 Truck vs. rail
 - 2.1.4 Relation to plant maintenance philosophy
 - 2.2 Solid vs. Aqueous Fuels

2.2.1 Hydrogen evolution from aqueous

- 2.3 Thermal Cooling
 - 2.3.1 Evaporation from aqueous
- 2.4 Capacity and Shielding

Fig.: Carrier for Radioactive Materials

2.4.1 Criticality

- 2.5 Mechanical Details
 - 2.5.1 Closure
 - 2.5.2 Stainless steel lining for ease of decontamination

2.5.3 George Parker's unitized construction

- 3.0 Viewing Devices
 - 3.1 Introduction
 - 3.1.1 Difficulties and limitations
 - a. Cell wall thickness
 - b. Contamination
 - c. You can't see through stainless steel anyway
 - d. Darkening of glass and other radiation damage
 - e. Expense
 - 3.1.2 Use for laboratories and small-scale facilities
 - 3.2 Methods Used
 - 3.2.1 Lead glass windows
 - a. Sampling stations ICPP, Thorex
 - b. RaLa centrifuge observation ICPP
 - 3.2.2 ZnBr, solution windows
 - a. Radioisotope separation
 - 3.2.3 Periscopes
 - a. Interface observation ORNL Pilot Plant
 - 3.2.4 Industrial TV
 - a. ORNL-VPP, HRT-CP

4.0 Manipulators

- 4.1 Introduction
 - 4.1.1 Seldom used in chemical plants
 - 4.1.2 Use in hot analytical
 - 4.1.3 Use in radioisotope separation

- 4.1.4 Use in development work
- 4.1.5 Potential use in mechanical handling
- 4.2 Types of Manipulators
 - 4.2.1 Master-Slave Fig.: Master-Slave Manipulator
 - 4.2.2 Mechanical-Rectilinear Fig.: Mechanical Hands
 - 4.2.3 Extraman

Fig.: Extraman

- 5.0 Samplers
 - 5.1 Introduction
 - 5.1.1 Representative sample
 - 5.1.2 Avoid cross-contamination
 - 5.1.3 Evaporation from own decay heat
 - 5.1.4 Hazards
 - 5.2 Samplers for Aqueous Solutions
 - 5.2.1 Recirculating airlift
 - a. Original design
 - b. Hypo needle-diaphragm refinement
 - c. Landry float
- Fig.: Recirculating Sampler for Aqueous Radioactive Solutions
- 5.2.2 Dip sampler RaLa, BiPOL, Redox
- 5.2.3 Remote pipet
- 5.2.4 HRT
- 5.2.5 Sample valve
- 5.3 Samplers for gases

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5.4 Samplers for Molten Salt

Fig.:

Sampler for Radioactive Molten Salt

Outline for Chapter XII

PLANT DESIGN

- 1.0 Preliminary Considerations
- 2.0 Process Design
- 3.0 Project Design
- 4.0 Hazards Study
- 5.0 Plant Start-up

1.0 Preliminary Considerations

- 1.1 Schematic Flow Sheet
 - 1.1.1 Sources of design information
 - 1.1.2 Major process steps and operating conditions
 - 1.1.3 Plant capacity
 - 1.1.4 Estimated space requirements

Fig.: Schematic Process Flow Sheet

1.2 Schedule

Fig.: Typical Plant Design Schedule

- 1.2.1 Process design
- 1.2.2 Project design
- 1.2.3 Fabrication
- 1.2.4 Construction
- 1.2.5 Start-up
- 1.3 Physical and Chemical Properties of Process Materials
- 1.4 Maintenance Philosophy
 - 1.4.1 Direct
 - 1.4.2 Remote

- 1.4.3 Underwater
- 1.4.4 Unit shielding
- 1.5 Location of Plant
 - 1.5.1 Radiological hazard to surroundings
 - 1.5.2 Proximity to reactor
 - 1.5.3 Accessibility to transportation
 - 1.5.4 Accessibility of utilities
 - 1.5.5 Accessibility of labor
- 1.6 Waste Disposal (solid, liquid and gaseous)
 - 1.6.1 Geological
 - 1.6.2 Seismological
 - 1.6.3 Meteorological
 - 1.6.4 Hydrological

2.0 Process Design

- 2.1 Process Flow Diagrams
- 2.2 Material Balance Flow Sheet
- 2.3 Energy Balance Flow Sheet
- 2.4 Preliminary Design of Main Components
 - 2.4.1 Size
 - 2.4.2 Number of nozzles and locations
 - 2.4.3 Instrumentation required
 - 2.4.4 Materials of construction

3.0 Project Design

3.1 Engineering Flow Diagrams

Fig.: Typical Engineering Flow Diagram

- 3.1.1 Equipment layout (elevation)
- 3.1.2 Process piping
- 3.1.3 Utilities
- 3.1.4 Electrical supply
- 3.1.5 Instrumentation
- 3.2 Detailed Engineering Design
 - 3.2.1 Vessel design
 - a. Capacity and major dimensions
 - b. Criticality
 - c. Decontamination
 - d. Materials of construction
 - e. Wall thickness
 - f. Welding specifications
 - g. Inspection specifications
 - h. Detailed construction drawings
 - 3.2.2 Equipment design
 - a. Detailed specifications on mechanical equipment
 - 3.2.3 Equipment and vessel layout
 - a. Plan and elevation drawings
 - 3.2.4 Instrumentation
 - 3.2.5 Piping design (process, instrument, air, water, conduit)
 - a. Inside cell
 - b. Outside cell
 - c. Wall penetrations
 - (1) Heat dissipation
 - (2) Radiation shielding

- d. Sizing
- e. Materials of construction
- f. Wall thickness
- g. Layout of various systems
- 3.2.6 Architectural
 - a. Plot plan
 - (1) Buildings
 - (2) Transportation
 - (3) Electrical substation
 - (4) Fuel element storage
 - (5) Waste storage
 - b. Main building
 - (1) Foundation
 - (2) Structural steel
 - (3) Cell wall
 - (4) Cell liners
 - (5) Cell drains
 - (6) Utilities
 - c. Auxiliary structures
 - (1) Analytical laboratory
 - (2) Machine shop
 - (3) Steam Plant
 - (4) Electrical substation
 - (5) Medical
 - (6) Health physics
 - (7) Stores

- (8) Decontamination Facilities
- (9) Plant Protection
- (10) Stack
- (11) Tank farm
- 3.2.7 Utilities
 - a. Steam
 - b. Process gases
 - (1) Air for spargers, jets, etc.
 - (2) Instrument air
 - (3) Blanket gases (N2, He, H2, 02, etc.)
 - c. Water
 - (1) Potable
 - (2) Distilled
 - (3) Process
 - d. Electricity
 - (1) Emergency power
 - e. Ventilation
 - (1) Off gas (cell)
 - (2) Off gas (vessel)
 - (3) Off gas (lab hoods)
 - (4) Vacuum
 - (5) Air conditioning for instruments
- 4.0 Hazards Study
 - 4.1 Nuclear Incident
 - 4.1.1 Possibility of inadvertent criticality
 - 4.2 Non-Nuclear Incident

4.2.1 Line break

a. Spread of radioactivity

4.2.2 Vessel leak

a. Spread of radioactivity

- 5.0 Plant Start-up
 - 5.1 Cleanliness
 - 5.1.1 Importance
 - 5.1.2 During construction
 - 5.1.3 After construction
 - 5.2 Leak Testing
 - 5.3 Vessel and Instrument Calibration
 - 5.4 Initial Component Operation

5.4.1 Heat transfer coefficients on jacketed tanks

- 5.4.2 Jets
- 5.4.3 Pumps
- 5.4.4 Column
- 5.4.5 Evaporation
- 5.4.6 Samplers
- 5.4.7 Others
- 5.5 Cold Runs

5.5.1 Process simulated except for radioactivity

- 5.6 Hot Runs
 - 5.6.1 Tracer
 - 5.6.2 1% activity
 - 5.6.3 10% activity
 - 5.6.4 100% activity

Outline for Chapter XIII

PLANT OPERATION

A.

- 1.0 General Considerations
- 2.0 Management
- 3.0 Operations
- 4.0 Analytical Operations
- 5.0 S. S. Accountability
- 6.0 Health Physics
- 7.0 Plant Protection
- 8.0 Maintenance
- 9.0 Utilities
- 10.0 Stores
- 1.0 General Considerations
 - 1.1 Value of Process Material

1.1.1 Seriousness of losses

- 1.2 Radioactivity of Process Materials
 - 1.2.1 Remote operation
 - 1.2.2 Effect on plant design
 - 1.2.3 Toxicity
- 1.3 Criticality

1.3.1 Effect on operation

- 1.3.2 Batch and concentration control
- 1.4 Investment in Plant and Operational Costs

1.4.1 Capacity operation desirable

1.4.2 Costly chemical reagents

- 2.0 Management
 - . 2.1 Organization and Scope
- 3.0 Operations
 - 3.1 Purpose and Scope
 - 3.2 Training
 - 3.3 Safety Program
- 4.0 Analytical Operations
 - 4.1 Purpose and Scope
 - 4.2 Special Techniques
- 5.0 S. S. Accountability
 - 5.1 Purpose and Scope
 - 5.2 Records Kept
- 6.0 Health Physics
 - 6.1 Purpose and Scope
 - 6.2 Records Kept
- 7.0 Plant Protection
 - 7.1 Purpose and Scope
 - 7.2 Organization
- 8.0 Maintenance
 - 8.1 Effect on Design
 - 8.2 Cold
 - 8.3 Hot

- 8.3.1 Direct
- 8.3.2 Remote
- 8.3.3 Underwater

9.0 Utilities

- 9.1 Emergency Sources
- 10.0 Stores

Outline for Chapter XIV

FUEL REPROCESSING ECONOMICS

- 1.0 General Considerations
- 2.0 The Nuclear Fuel Cycle
- 3.0 Chemical Reprocessing in the Nuclear Fuel Cycle
- 4.0 Economic Comparison of Various Fuel Reprocessing Methods
- 5.0 Factors Affecting Reprocessing Costs

1.0 General Considerations

- 1.1 Value of Uranium and Thorium
- 1.2 Supply of Uranium and Thorium
- 2.0 The Nuclear Fuel Cycle
 - 2.1 Definition

Fig.: "Typical Heterogeneous Fuel Cycle"

- 2.2 Comparison with Conventional Fuel Cycle
- 2.3 Effect of Fuel Cycle on Power Costs
 - 2.3.1 Nuclear
 - 2.3.2 Conventional

3.0 Chemical Reprocessing in the Nuclear Fuel Cycle

- 3.1 Purpose
 - 3.1.1 Recover fissionable material
 - 3.1.2 Decontaminate fissionable material
- 3.2 Cost of Chemical Reprocessing Relative to Other Steps

- 4.0 Economic Comparison of Various Fuel Reprocessing Methods
 - 4.1 Introduction
 - 4.2 Cooling Costs
 - 4.3 Head End Treatment Costs

4.3.1 U-Al in HNO2

a. Acid recovery

- 4.3.2 U-Al in NaOH
- 4.3.4 Th-Al in HNO3
- 4.3.5 U-Zr in aqueous HF-HNO2
- 4.3.6 U-Zr by HF in fused salt
- 4.3.7 U-SS in dilute aqua regia
- 4.3.8 U-SS in H2S04
- 4.3.9 ThO2 in HNO3
- 4.4 Precipitation Process Costs
 - 4.4.1 BiPO
 - 4.4.2 MCFPPP (Multicurie Fission Product Pilot Plant)
 - 4.4.3 RaLa
- 4.5 Solvent Extraction Process Costs
 - 4.5.1 Extraction
 - 4.5.2 Partition
 - 4.5.3 Second uranium cycle
 - 4.5.4 Second plutonium cycle
 - 4.5.5 Third uranium cycle
 - 4.5.6 Intercycle evaporation
 - 4.5.7 Plutonium isolation
 - 4.5.8 Solvent recovery

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- 4.6 Volatility Costs
 - 4.6.1 Volatilization
 - 4.6.2 Adsorption
 - 4.6.3 Distillation
 - 4.6.4 UF6 recovery
 - 4.6.5 Fluorine disposal
- 4.7 Tail End Treatment Costs
 - 4.7.1 UNH to UO_3 4.7.2 UO_3 to UF_4 4.7.3 UF_4 to UF_6 4.7.4 UF_6 to U4.7.5 UF_4 to U
- 4.8 Waste Disposal Costs
 - 4.8.1 Gas
 - 4.8.2 Liquid
 - 4.8.3 Solid
- 4.9 Integrated Process Costs
- 5.0 Factors Affecting Reprocessing Costs
 - 5.1 Plant Capacity
 - 5.2 Transportation
 - 5.3 Burnup
 - 5.4 Cooling Time
 - 5.5 Transuranics
 - 5.6 Breeding
 - 5.7 Waste Disposal

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