DOE/FE-0387

CLEAN COAL TECHNOLOGY

Clean Coal Technology Demonstration Program

Program Update 1998

U.S. Department of Energy
Assistant Secretary for Fossil Energy
Washington, DC 20585

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Introduction

The Clean Coal Technology Demonstration Program (CCT Program), a model of government and industry cooperation, responds to the Department of Energy's (DOE) mission to foster a secure and reliable energy system that is environmentally and economically sustainable. With 23 of the 40 active projects having completed operations, the CCT Program has yielded clean coal technologies (CCTs) that are capable of meeting existing and emerging environmental regulations and competing in a deregulated electric power marketplace.

The CCT Program is providing a portfolio of technologies that will assure the U.S. recoverable coal reserves of 274 billion tons can continue to supply the nation's energy needs economically and in an environmentally sound manner. As the new millennium approaches, many of the clean coal technologies have realized commercial application. Industry stands ready to respond to the energy and environmental demands of the 21st century, both domestically and internationally. For existing power plants, there are cost effective environmental control devices to control sulfur dioxide (SO_2), nitrogen oxides (NO_x), and particulate matter (PM). Also ready are a new generation of technologies that can produce electricity and other commodities, such as steam and synthetic gas, and provide the efficiencies and environmental performance responsive to global climate change. The CCT Program took a pollution prevention approach as well, demonstrating technologies that produce clean coal-based solid and liquid fuels by removing pollutants or their precursors. Lastly, new technologies were introduced into the major coal-using industries to enhance environmental performance. Thanks in part to the CCT Program, coal—abundant, secure, and economical—can continue in its role as a key component in the U.S. and world energy markets.

Role of the CCT Program

Coal Technologies Respond to Need. Coal accounts for over 94 percent of the proven fossil energy reserves in the United States and supplies the bulk of the low-cost reliable electricity vital to the nation's economy and global competitiveness. In 1996, over half of the nation's electricity was produced with coal and projections by the Energy Information Agency (EIA) predict that coal will continue to dominate electric power production well into the first quarter of the 21st century. However, there is also a need to use U.S. coal resources in an environmentally responsible manner. The CCT Program responds to both of these needs.

The CCT Program was established to demonstrate the commercial feasibility of CCTs to respond to a growing demand for a new generation of advanced coal-based technologies characterized by enhanced operational, economic, and environmental performance. The first solicitation (CCT-I) for clean coal projects resulted in a broad range of projects being selected in four major product markets–environmental

▼ Tidd PFBC Demonstration Project (The Ohio Power Company)—1991 Powerplant Award presented by *Power* magazine.

▲ Tampa Electric Integrated Gasification Combined-Cycle Project (Tampa Electric Company)—1997 Powerplant Award presented by *Power* magazine.

control devices, advanced electric power generation, coal processing for clean fuels, and industrial applications.

The second round of solicitations (CCT-II) became the centerpiece for satisfying the recommendations contained in the Joint Report of the Special Envoys on Acid Rain (1986). The goal was to demonstrate technologies that could achieve significant reductions in the emissions of precursors of acid rain, namely SO_2 and NO_x. The third round of solicitations (CCT-III) furthered the goal of CCT-II and added technologies that could produce clean fuel from run-of-mine coal.

The fourth and fifth solicitations (CCT-IV and CCT-V, respectively) recognized emerging energy and environmental issues, such as global climate change and capping SO_2 emissions, and thus focused on technologies that were capable of addressing these issues. CCT-IV called for energy efficient economically competitive technologies capable of retrofitting, repowering, or replacing existing facilities, while at the same time significantly reducing SO_2 and NO_x emissions. CCT-V focused on technologies applicable to new or existing facilities that could significantly improve efficiency and environmental performance.

Coal Technologies for Environmental Performance. Even before enactment of the Clean Air Act Amendments of 1990 (CAAA), the CCT Program was cognizant of the changes in electric power generation that would likely be caused by the statute. Several projects in the CCT Program were implemented at units designated as Phase I units in Title IV of the CAAA, which were required to meet SO_2 reductions by January 1, 1995. The CCT Program projects at Phase I units successfully reduced SO_2 emissions using advanced flue gas desulfurization (AFGD) and repowering with integrated gasification combined cycle (IGCC). With a January 1, 2000 deadline quickly approaching for Phase II of Title IV, the CCT Program has developed a portfolio of technologies that will help industry meet the more stringent SO_2 emission limits. Unit operators now have several options for meeting SO_2 limitations or exceeding them to generate SO_2 credits that can be sold in the emissions credit market. Furthermore, these SO_2 reduction technologies may be important in meeting new requirements for $PM_{2.5}$ (particulate matter 2.5 microns and smaller in diameter) because some sulfur species are also $PM_{2.5}$.

In addition to SO_2 reductions, Title IV also called for reductions in NO_x emissions. Phase I of the NO_x provisions of Title IV requires reductions from the so-called Group 1 boilers–tangentially-fired and dry-bottom wall-fired boilers. The Environmental Protection Agency (EPA) used data developed during the CCT Program in establishing the NO_x emission standards. Under Phase II, EPA established NO_x emission limitations for Group 2 boilers and reduced the emission limits for Group 1 boilers. Group 2 boilers include cell-burner, cyclone, wet-bottom wall-fired, and vertically-fired boilers. The CCT Program has demonstrated NO_x emission techniques that are applicable to all of these boiler types. Furthermore, these technologies are not only applicable to Phase I and II NO_x emission reductions, but can be used in ozone nonattainment areas to make deeper cuts in NO_x, which is a precursor to ozone.

▼ Demonstration of Innovative Applications of Technology for the CT-121 FGD Process Project (Southern Company Services, Inc.)—1994 Powerplant Award presented by *Power* magazine.

The issue of ozone nonattainment has recently taken on new proportions as EPA has issued a “SIP Call” to 22 states and the District of Columbia to take action to reduce regional transport of pollutants that contribute to ozone nonattainment in the Northeast. The SIP Call requires the 23 affected jurisdictions to revise their state implementation plans (SIP) to reduce NO_x emissions 85 percent below 1990 rates or achieve a 0.15 lb/10^6 Btu emission rate by May 2003. In addition, EPA has tightened the New Source Performance Standard (NSPS) for electric and industrial boilers built or modified after July 9, 1997. The CCT Program has demonstrated several advanced electric power generation technologies that can be used to meet the new requirements or exceed the requirements to produce NO_x credits that could be sold to unit operators unable to meet the requirements. Furthermore, an environmental controls database has been developed that provides a foundation for meeting the increasingly stringent standards for existing units.

Air toxics is another important area of environmental concern addressed by the CCT Program. Under Title I of the CAAA, EPA is responsible for determining the hazards to public health posed by 189 identified hazardous air pollutants (HAPs). The CCT Program made a significant contribution to a better understanding of potential HAPs from power plant emissions by monitoring HAPs from CCT Program project sites. The results of these and other studies have significantly mitigated concerns about HAP emissions from coal-fired power plants and focused attention on only a few flue gas constituents.

The CCT Program is also cognizant of concerns about global climate change. Clean coal technology, such as IGCC, being demonstrated in the CCT Program offers utilities an option to reduce greenhouse gases (GHG) by as much as 25 percent with first generation systems through enhanced efficiency. Commercialization of atmospheric fluidized-bed combustion (AFBC) and pressurized fluidized-bed combustion (PFBC) will also serve to reduce GHGs.

Coal Technologies for Competitive Performance. As the electric generation market moves from a regulated industry to a free market, the CCT Program has kept pace with the changes. Whether the changes are brought about by the federal government through existing or new legislation or by state governments, the CCT Program is demonstrating the first generation of many technologies that will be needed in a competitive power generation market. These new technologies will be far more efficient than existing plants and environmentally benign.

Coal Technologies to Sustain Economic Growth. It is in the nation's interest to maintain a diverse energy mix to sustain domestic economic growth. The CCT Program is contributing to this interest by developing and deploying a technology portfolio that enhances the efficient use of the United States' abundant natural resource while simultaneously achieving important environmental goals. The advancements in use of coal resulting from the CCT Program will reduce dependance on foreign energy resources and create an international market for these new technologies.

Coal Technology for the Future. The Department of Energy's Office of Coal and Power Systems (OC&PS) Research, Development, and Demonstration (RD&D) Program is building on the CCT Program to develop a "Vision 21 PowerPlex." This Vision 21 PowerPlex is a modular facility using a multiplicity of fuels to produce a variety of commodities (electricity, steam, fuels, and chemicals) at efficiencies exceeding 60 percent and with near zero emissions. Vision 21 PowerPlex systems will build upon the clean coal technologies and attendant databases developed in the CCT Program in meeting the goals established for the 21st century.

▲ Advanced Flue Gas Desulfurization Demonstration Project (Pure Air on the Lake, L.P.)—1993 Powerplant Award presented by *Power* magazine.

Program Implementation

Implementation Principles. There are 10 guiding principles that have been instrumental in the success of the CCT Program. These are:

- strong and stable financial commitment for the life of the project, including full funding of the government's share of the costs;
- multiple solicitations spread over a number of years, enabling the CCT Program to address a broad range of national needs with a portfolio of evolving technologies;
- demonstrations conducted at commercial scale in actual user environments, allowing clear assessment of the technology's commercial potential;
- a technical agenda established by industry, not the government, enhancing commercialization potential;
- clearly defined roles of government and industry, reflecting the degree of cost sharing required;
- a requirement for at least 50 percent cost sharing throughout all project phases, enhancing participant's commitment;
- an allowance for cost growth, but with a ceiling and cost-sharing, recognizing demonstration risk and providing an important check-and-balance to the program;
- industry retains real and intellectual property rights, enhancing commercialization potential;
- a requirement for industry to commit to commercialize the technology, reflecting commercialization goals; and
- a requirement for repayment up to the government's cost share upon successful commercialization of the technology being demonstrated, reflecting DOE policy.

Implementation Process. Public and private sector involvement is integral to the CCT Program process and was crucial to the program's success. Environmental concerns are publicly addressed through the process instituted under the National Environmental Policy Act (NEPA). Through programmatic environmental assessments (PEAs), environmental impact statements (EISs), project specific Environmental Assessments (EAs) and EISs, and other NEPA documents, the public is able to comment and have their comments addressed before the projects proceed to implementation. In addition, environmental monitoring programs are required for all projects to address non-regulated pollutant emissions.

As to the solicitation process, Congress set the goals for each solicitation. The Department of Energy translated the congressional guidance into performance-based criteria and developed approaches to address "lessons learned" from previous solicitations. The criteria and solicitation procedures were offered for public comment and presented at pre-proposal conferences. The solicitations were objectively evaluated against the pre-established criteria.

Projects are managed by the participants, not the government. However, to protect the public interest, safeguards are implemented to track and monitor project progress and direction. The Department of Energy interacts with the project at key negotiated decision points (budget periods) to approve or disapprove continuance of the project. Also, any changes to cost or other major project changes require DOE approval. In addition to formal project reporting requirements, an outreach program was instituted to make project information available to customers and stakeholders. This *Program Update 1998* is only one of the many public reports made available through the outreach program.

Commitment to Commercial Realization. The CCT Program has focused on achieving commercial realization since the program's inception. All five solicitations required the potential participant to address the commercial plans and approaches to be used by the participant to achieve full commercialization of the proposed technology. The cooperative agreement contained balanced provisions that provide protection for intellectual property but required the participant to make the technology available under license on a nondiscriminatory basis.

Solicitation Results. Each solicitation was issued as a Program Opportunity Notice (PON)—a solicitation mechanism for cooperative agreements where the program goals and objectives are defined, but the technology is not defined. The procurements followed specific statutory requirements that would eventually lead to a cooperative agreement between DOE and the participant. The result was a broad spectrum of technologies involving customers and stakeholders from all market segments. In sum, 211 proposals were submitted and 60 of those were selected. As of September 1998, a total of 40 projects have been completed or are currently active. These 40 projects are spread across the nation in 18 states.

Future Implementation Direction. The future direction of the CCT Program focuses on completing the existing projects as promptly as possible and assuring the collection, analyses, and reporting of the operational, economic, and environmental performance results that are needed to affect commercialization. In FY1999, the Clean Coal Diesel Demonstration project is scheduled to begin operations. Five projects are scheduled to complete operations in FY1999.

The body of knowledge obtained as a result of the CCT Program is being used in decisionmaking relative to regulatory compliance, forging plans for meeting future energy and environmental demands, and developing the next generation of technologies responsive to ever increasing demands on environmental performance at competitive costs. Three major drivers will affect implementation of the CCT Program—environmental concerns, utility restructuring, and the international market—because of their impact on market entry and deployment of clean coal technologies.

Environmental concerns include regional NO_x transport impacting ozone nonattainment areas, $PM_{2.5}$, and global climate change. Utility restructuring from a regulated industry to a market-based industry will require new clean coal technologies to be cost effective and have a technological risk comparable to conventional technologies. The international market shows the greatest near-term market potential for clean coal technologies. With more than 50 percent future demand for new generation between now and 2010 coming from Asia, there is a tremendous market potential for clean coal technologies that can use indigenous fuels.

Funding and Costs

Program Funding. Congress has appropriated a federal budget of $2.3 billion for the CCT Program. For the 40 completed and active projects, the participants have contributed $3.7 billion dollars for a combined commitment of more than $5.6 billion. By law, DOE's contribution can not exceed 50 percent of the total cost of any project. However, industry has stepped forward and cost shared an unprecedented 66 percent of the project funding.

Congress has provided CCT Program funding for all five solicitations through appropriation acts and adjustments. Additional activities funded by the CCT Program are the Small Business Innovation Research Program and the Small Business Technology Transfer Program. Funding is also provided for administration and management of the CCT Program. Use of appropriated funds are controlled and monitored using a variety of financial management techniques. The full government cost share specified in the cooperative agreement is considered committed to each project; however, DOE obligates funds for the project in increments by budget period. This procedure reduces the government's financial exposure and assures that DOE fully participates in the decision to proceed with each major phase of project implementation.

Cost Sharing. As stated above, DOE's contribution can not exceed 50 percent of the total cost of any project. This cost sharing is required for all phases of the project. The federal government may share in project cost growth (which, by its very nature, is likely to happen for any demonstration project) up to 25 percent of the original project cost. The participant's contributions must occur as expenses are incurred and can not be delayed based on forecasted revenues, proceeds, or royalties. Also, prior investments in facilities by participants can not count towards the participant's share.

Recovery of Government Outlays (Recoupment). The policy objective of DOE is to recover an amount up the federal government's financial contribution to each project when a technology is successfully commercialized. Participants are required to submit a plan outlining a proposed schedule for recoupment. Each of the five solicitations have featured different sets of recoupment rules because of lessons learned from prior solicitations.

CCT Program Accomplishments

Marketplace Commitment. The success of the CCT program ultimately will be measured by the contribution the technologies make to the resolution of energy, economic, and environmental issues. These contributions can only be achieved if the public and private sectors understand that clean coal technologies can increase the efficiency of energy use and enhance environmental performance at costs that are competitive with alternative energy options. The CCT Program is organized from a market perspective with projects placed in four major product lines—environmental control devices, advanced electric power generation, coal processing for clean fuels, and industrial applications. A summary of the number of projects having completed operations by category is shown in Exhibit ES-1.

The first major product line, environmental control devices, is subdivided into three groups—SO_2 control technologies, NO_x control technologies, and combined SO_2/NO_x control technologies. Both wet and dry lime- and limestone-based systems were demonstrated to achieve a range of SO_2 capture efficiencies of 50 to 99 percent. All five of the SO_2 control technology demonstrations have successfully completed operations.

For NO_x control technologies, two basic approaches were used: (1) combustion modification techniques using low NO_x burners and reburning systems, and (2) post-combustion techniques using selective catalytic reduction (SCR) and selective non-catalytic reduction (SNCR) systems. These NO_x control techniques were applied in a variety of combinations on a variety of boilers, which are representative of 90 percent of the pre-NSPS boilers, i.e., those boilers built before NSPS were imposed by the Clean Air Act of 1970. The result of the NO_x control technology demonstrations is a

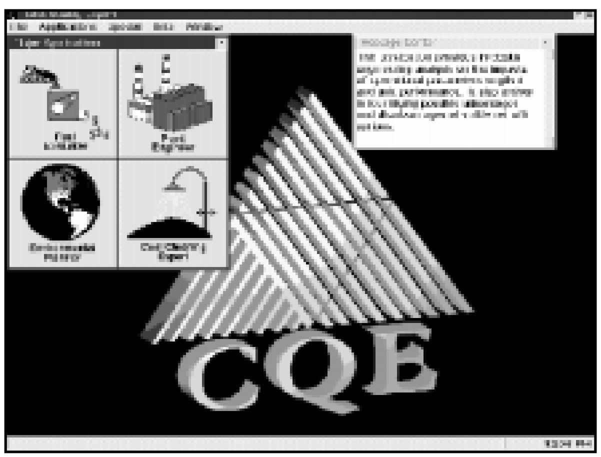
Exhibit ES-1
Completed Projects by Application Category

Application Category	Number of Projects: Completed Operations	Total
Environmental Control Devices		
SO_2 Control Technology	5	5
NO_x Control Technology	6	7
Combined SO_2/NO_x Control Technology	6	7
Advanced Electric Power Generation		
Fluidized-Bed Combustion	2	5
Integrated Gasification Combined Cycle	0	4
Advanced Combustion/Heat Engines	0	2
Coal Processing for Clean Fuels	2	5
Industrial Applications	2	5
Total	**23**	**40**

portfolio of technologies that can be used to address today's pressing environmental concerns, e.g., ozone. Six of the seven NO_x control technology demonstrations have successfully completed operations.

Six of the seven combined SO_2/NO_x control technology demonstrations have successfully completed operations. The demonstrations tested a multiplicity of complementary and synergistic control methods to achieve cost-effective SO_2 and NO_x emission reductions. A summary of the results of the completed environmental control device projects can be found in Exhibit ES-2. The commercial successes of the environmental control devices can be seen in Exhibit ES-3.

The second major product line, advanced electric power generation, is subdivided into three groups–(1) fluidized-bed combustion, (2) integrated gasification combined-cycle, and (3) advanced combustion/heat engines. These technologies can be used for repowering existing generation and new generation.



▲ Development of the Coal Quality Expert™ Project (ABB Combustion Engineering, Inc., and CQ Inc.)—1996 recognized by Secretary of Energy and EPRI as one of best cost-shared utility projects.

For fluidized-bed combustion, two approaches were used: atmospheric fluidized-bed combustion (AFBC) and pressurized fluidized-bed combustion (PFBC). The two AFBC projects demonstrated in the CCT Program used a circulating-bed, as opposed to a bubbling-bed, operating at atmospheric pressure to generate steam for electricity production. One project is complete and the other project is ongoing. There are three PFBC projects in the CCT Program. One PFBC project used a bubbling-bed operating at 16 atmospheres to generate steam and drive a gas turbine in a combined-cycle mode. Two ongoing interrelated PFBC projects will use a circulating-bed operating at 13 atmospheres, also in a combined-cycle mode.

Three of the four integrated gasification combined cycle demonstration projects are in various stages of operation. A fourth project is in the design stage. The IGCC projects represent a diversity of gasifier types, cleanup systems, and applications.

Two projects are demonstrating advanced combustion/heat engine technology. One uses an entrained (slagging) combustor and the other uses a heavy duty diesel fired on a coal-water fuel. Both of these projects are ongoing.

A summary of the results of the completed advanced electric power generation projects can be found in Exhibit ES-4. The commercial successes of these projects can be seen in Exhibit ES-5.

For the third major product line, coal processing for clean fuels, there are five projects. Three projects are using chemical and physical processes to transform raw coal into an environmentally compliant fuel. Another project is using coal to produce methanol from coal-derived synthesis gas. A fifth project in this product line is a software program used to assess the environmental and operational performance and determine the least-cost option for available coals. Two of the five coal processing for clean fuels projects are complete.

A summary of the results of the completed coal processing for clean fuels projects can be found in

▲ Wabash River Coal Gasification Repowering Project (Wabash River Coal Gasification Repowering Project Joint Venture)—1996 Powerplant Award presented by *Power* magazine.

▲ Full-Scale Demonstration of Low-NO_x Cell Burner Retrofit Project (The Babcock & Wilcox Company)—1994 R&D 100 Award presented by *R&D* magazine.

Exhibit ES-2
Summary of Results of Completed Environmental Control Technology Projects

Project and Participant	Key Results	Capital Cost
SO_2 Control Technology		
10-MWe Demonstration of Gas Suspension Absorption (AirPol, Inc.)	Gas suspension absorption (GSA)/electrostatic precipitator (ESP)—SO_2 removal efficiency of 90% at Ca/S molar ratio of 1.4, 18 ºF approach to saturation, and 0.12% chloride GSA/pulse jet baghouse—SO_2 removal efficiency 3–5% greater than GSA/ESP (3.0% sulfur bituminous coal)	\$149/kW for GSA, (2-6% sulfur coal) (\$216/kW for conventional wet limestone forced oxidation) (1990\$)
Confined Zone Dispersion Flue Gas Desulfurization Demonstration (Bechtel Corporation)	SO_2 reduction of 50% (1.2–2.5% sulfur bituminous coal)	Less than \$30/kW at 500 MWe (4% sulfur coal)
LIFAC Sorbent Injection Desulfurization Demonstration Project (LIFAC–North America)	SO_2 removal efficiency of 70% at 2.0 Ca/S molar ratio (2.0–2.8% sulfur bituminous coal)	\$66/kW for two reactors (300 MWe); \$76/kW for one reactor (150 MWe); \$99/kW for one reactor (65 MWe)
Advanced Flue Gas Desulfurization Project (Pure Air on the Lake, L.P.)	SO_2 removal efficiency of 95% or more at availabilities of 99.5% when operating on 2.0–4.5% sulfur bituminous coal Maximum SO_2 removal efficiency of 98% Over 3-year demonstration, 237,000 tons of SO_2 removed while producing 210,000 tons of gypsum Gypsum purity—97.2% Power consumption—5,275 kW (61% of expected) Water consumption—1,560 gal/min (52% of expected)	\$210/kW at 100 MWe; \$121/kW at 300 MWe; \$94/kW at 500 MWe (3.0% sulfur coal) (1995\$)
Demonstration of Innovative Applications of Technology for the CT-121 FGD Process (Southern Company Services, Inc.)	SO_2 removal efficiency of over 90% at SO_2 inlet concentrations of 1,000–3,500 ppm Particulate removal efficiency of 97.7–99.3% at inlet mass loadings of 0.303–1.392 lb/10^6 Btu Produced wallboard-grade gypsum as a by-product Fiberglass-reinforced-plastic equipment—chemically and structurally durable; eliminating the need for a flue gas prescrubber and reheat	Not yet available

Exhibit ES-2 (continued)
Summary of Results of Completed Environmental Control Technology Projects

Project and Participant	Key Results	Capital Cost
NO_x Control Technology		
Demonstration of Coal Reburning for Cyclone Boiler NO_x Control (The Babcock & Wilcox Company)	NO_x reductions of 52% using bituminous coal and 55% using subbituminous coal at full load (110 MWe); 36% and 53%, respectively, at 60 MWe	\$66/kW at 110 MWe; \$43/kW at 605 MWe (1990\$)
Full-Scale Demonstration of Low-NO_x Cell Burner Retrofit (The Babcock & Wilcox Company)	NO_x reductions of 54–58% using bituminous coal at full load (605 MWe); 48% at 350 MWe	\$9/kW at 600 MWe (1994\$)
Evaluation of Gas Reburning and Low-NO_x Burners on a Wall-Fired Boiler (Energy and Environmental Research Corporation)	LNB alone (second generation)—37% NO_x reduction; GR–LNB (second generation)—64% NO_x reduction (13% gas heat input)	Approximately \$15/kW for gas reburning, plus gas pipeline cost (1996\$)
Demonstration of Selective Catalytic Reduction Technology for Control of NO_x Emissions from High-Sulfur-Coal-Fired Boilers (Southern Company Services, Inc.)	NO_x reductions of over 80% at ammonia slip well under 5 ppm	Levelized cost at 80% NO_x reduction— 2.79 mills/kWh or \$2,036/ton of NO_x removed (1996\$)
180-MWe Demonstration of Advanced Tangentially Fired Combustion Techniques for Reduction of NO_x Emissions from Coal-Fired Boilers (Southern Company Services, Inc.)	NO_x reductions of 37% for LNCFS™ I and II, and 45% for LNCFS™ III, which includes both separated overfire air and close-coupled overfire air	LNCFS I—\$5–15/kW (1993\$) LNCFS II/III—\$15–25/kW (1993\$)
Demonstration of Advanced Combustion Techniques for a Wall-Fired Boiler (Southern Company Services, Inc.)	Using LNB alone, NO_x emissions were 0.65 lb/10^6 Btu at full load, representing a 48% reduction from baseline conditions (1.24 lb/10^6 Btu) Using AOFA only, NO_x reductions of 24% below baseline conditions were achieved under normal long-term operation, depending upon load Using LNB/AOFA, full load NO_x emissions were approximately 0.40 lb/10^6 Btu, which represents a 68% reduction from baseline conditions	Capital cost for a 500 MWe wall-fired unit is \$8.8/kW for AOFA alone, \$10.0/kW for LNB alone, and \$0.5/kW GNOCIS Estimated cost of NO_x removal is \$86/ton
Combined SO_2/NO_x Control Technology		
SNOX™ Flue Gas Cleaning Demonstration Project (ABB Environmental Systems)	NO_x reduction with SCR over 94% at inlet concentrations of 500–700 ppm SO_2 removal efficiency over 95% at inlet concentrations of 2,000 ppm Produced salable sulfuric acid by-product	\$305/kW at 500 MWe (3.2% sulfur coal) (1995\$)

Exhibit ES-2 (continued)
Summary of Results of Completed Environmental Control Technology Projects

Project and Participant	Key Results	Capital Cost
LIMB Demonstration Project Extension and Coolside Demonstration (The Babcock & Wilcox Company)	SO_2 removal efficiency (3.8% sulfur coal, Ca/S molar ratio of 2.0): LIMB—53–61% for ligno lime, 51–58% for calcitic lime Coolside—70% for hydrated lime NO_x reduction of 40–50%	LIMB—$31–102/kW (100–500 MWe) Coolside—$69–160/kW (100–500 MWe)
SO_x-NO_x-Rox Box™ Flue Gas Cleanup Demonstration Project (The Babcock & Wilcox Company)	SO_2 reductions of 80–90% using 3–4% sulfur bituminous coal, depending on sorbent and conditions NO_x reduction of 90% with 0.9 NH_3/NO_x ratio	$233/kW at 250 MWe (3.5% sulfur coal and inlet NO_x level of 1.2 lb/10^6 Btu) (1994$)
Enhancing the Use of Coals by Gas Reburning and Sorbent Injection (Energy and Environmental Research Corporation)	Hennepin—NO_x reduction of 67% avg with 18% gas input; SO_2 removal efficiency of 53% at 1.75 Ca/S molar ratio Lakeside—NO_x reduction of 66% avg and SO_2 reductions of 58% during extended continuous combined (GR–SI) runs at 29 MWe, about 22% gas input, and 1.8 Ca/S molar ratio	$15/kW for gas reburning, plus gas pipeline cost $50/kW for sorbent injection
Milliken Clean Coal Technology Demonstration Project (New York State Electric & Gas Corporation)	The maximum SO_2 removal demonstrated has been 98% with all seven recycle pumps operating and using formic acid. The maximum SO_2 removal without formic acid has been 95% Testing of the LNCFS™ III indicated NO_x emissions of 0.39 lb/10^6 Btu (compared to 0.61 lb/10^6 Btu for the original burners)	Not yet available
Integrated Dry NO_x/SO_2 Emissions Control System (Public Service Company of Colorado)	NO_x reduction of 67% avg during long-term testing of gas reburning only NO_x reduction of 62–69% with low-NO_x burners and maximum overfire air (50–110 MWe) NO_x reduction of 63% with low-NO_x burners and minimum overfire air; steady state conditions NO_x reduction decreased by 10–25% under load following SNCR obtained NO_x reduction of 30–50%, thereby increasing total NO_x control system reduction to more than 80% SO_2 removal efficiency of 70% with sodium bicarbonate at normalized stoichiometric ratio of 1.0	Not yet available

Exhibit ES-3
Commercial Successes—Environmental Control Technologies

Project and Participant	Commercialization Progress
LIFAC Sorbent Injection Desulfurization Demonstration Project (LIFAC–North America)	Technology retained for commercial use at host site First high-sulfur coal application 10 commercial units in operation or construction (Canada, China, Finland, Russia, and U.S.)
10-MWe Demonstration of Gas Suspension Absorption (AirPol, Inc.)	Sale of 50-MWe unit to city of Hamilton, OH – Value—$10 million Sale to U.S. Army for hazardous waste disposal – Value—$1.3 million Sale to Sweden for iron ore sinter plant (no value available) Sales to Taiwan and India – Combined value—$33 million Sale of technical assistance and proprietary equipment to Taiwan – Value—$1 million
Advanced Flue Gas Desulfurization Demonstration Project (Pure Air on the Lake, L.P.)	Technology retained for commercial use at host site; first scrubber to comply with CAAA installed; Wallboard manufacturer using all gypsum produced
Demonstration of Innovative Applications of Technology for the CT-121 FGD Process (Southern Company Services, Inc.)	Technology retained for commercial use at host site Since the CCT Program demonstration, over 8,200 MWe equivalent of CT-121 FGD capacity has been sold to 16 customers in seven countries
Demonstration of Coal Reburning for Cyclone Boiler NO_x Control (The Babcock & Wilcox Company)	Technology retained for commercial use at host site
Full-Scale Demonstration of Low-NO_x Cell Burner Retrofit (The Babcock & Wilcox Company)	Technology retained for commercial use at host site Seven commercial contracts awarded for 144 burners – Value—$27 million
Evaluation of Gas Reburning and Low-NO_x Burners on a Wall-Fired Boiler (Energy and Environmental Research Corporation)	Technology retained for commercial use at host site
Demonstration of Advanced Combustion Techniques for a Wall-Fired Boiler (Southern Company Services, Inc.)	Technology retained for commercial use at host site Foster Wheeler has equipped 86 boilers with low NO_x technology (51 domestic and 35 international) – Quantity—1,800 burners for over 30,000 MWe capacity 19 GNOCIS neural-network control projects underway Expect another 17 GNOCIS projects in 1999 Organizations selected to market GNOCIS in U.S. and abroad

Exhibit ES-3 (continued)
Commercial Successes—Environmental Control Technologies

Project and Participant	Commercialization Progress
180-MWe Demonstration of Advanced Tangentially Fired Combustion Techniques (Southern Company Services, Inc.)	Technology retained for commercial use at host site ABB Combustion Engineering has modified 116 coal-fired tangentially-fired boilers, representing over 25,000 MWe, with LNCFS™ and TFS 2000™
SNOX™ Flue Gas Cleaning Demonstration Project (ABB Environmental Systems)	Technology retained for commercial use at host site 305-MWe unit operating in Denmark on coal 30-MWe unit operating in Sicily on petroleum coke
LIMB Demonstration Project Extension and Coolside Demonstration (The Babcock & Wilcox Company)	Sale of LIMB to independent power project in Canada
Enhancing the Use of Coals by Gas Reburning Sorbent Injection (Energy and Environmental Research Corporation)	Illinois Power and City Water, Light & Power retained gas reburning for commercial use
Milliken Clean Coal Technology Demonstration Project (New York State Electric & Gas Corporation)	Four sales of DHR Technologies' Plant Emission Optimization Advisor More than 20 NO_x OUT® or NO_x OUT® derivative units sold in U.S, Taiwan, and Korea U.S. company, SHN, established to market S-H-U scrubber Actively pursuing AFGD bid for Pennsylvania site (will include S-H-U process, Stebbins absorber module, and heat-pipe air preheater)
Integrated Dry NO_x/SO_2 Emissions Control System (Public Service Company of Colorado)	Technology retained for commercial use at host site Sales of Babcock & Wilcox DRB-XCL® low-NO_x burners (which are components of the technology demonstrated) – Quantity—2,428 burners for 31,467 MWe capacity – Value—$320 million

Exhibit ES-6. The commercial successes of the coal processing for clean fuels projects can be seen in Exhibit ES-7.

The fourth and final major product line is industrial applications. This product line is addressing the environmental issues and barriers associated with coal use in industry. There are five diverse projects in this category; two are completed and three are ongoing. A summary of the results of the completed industrial application projects can be found in Exhibit ES-8. The commercial successes of these projects can be seen in Exhibit ES-9.

Market Communications–Outreach. Outreach has been a hallmark of the CCT Program since it's inception. Commercialization of new technologies requires acceptance by a wide range of interests– customers, manufacturers, suppliers, financiers, government, and public interest groups. The CCT Program has aggressively sought to disseminate key information to this full range of customers and stakeholders and to obtain feedback on changing needs. This dissemination of information takes the form of printed media, exhibits, and electronic media. Printed media takes the form of newsletters, proceedings, technical papers, fact sheets, program updates, and bibliographies. The CCT Program currently uses four traveling exhibits of varying sizes and complexity that can be updated and tailored to specific forums. Electronic media is available through fax-on-demand, computer bulletin board system, and the World Wide Web. As the 21st century

Exhibit ES-4
Summary of Results of Completed Advanced Electric Power Generation Projects

Project and Participant	Key Results	Capital Cost
Tidd PFBC Demonstration Project (The Ohio Power Company)	SO_2 reduction of 90–95% (Ohio bituminous coal, 2–4% sulfur) at 1.1–1.5 Ca/S molar ratio NO_x emissions of 0.15–0.33 lb/10^6 Btu Particulate emissions of 0.02 lb/10^6 Btu Heat rate—10,280 Btu/kWh Combustion efficiency—99.6% Commercially viable design Gas turbine operable in PFBC environment	$1,263/kW at 360 MWe (1997$)
Nucla CFB Demonstration Project (Tri-State Generation and Transmission Association, Inc.)	SO_2 reduction of 70–95% (up to 1.8% sulfur coal), depending on Ca/S molar ratio NO_x emissions of 0.18 lb/10^6 Btu avg Particulate emissions of 0.0072–0.0125 lb/10^6 Btu avg Heat rate—11,600 Btu/kWh Combustion efficiency—96.9–98.9% Commercial viability established	Approximately $1,123/net kW (repower cost)

approaches, DOE is making more information available via the World Wide Web.

Feedback is another important part of the outreach program. From public meetings during the PON process to open houses at demonstration sites, the CCT Program stays in contact with customers and stakeholders. Executive seminars, stakeholder meetings, conferences, workshops, and trade missions are used by the CCT Program to disseminate information and obtain feedback. The premier CCT Program outreach events are the annual clean coal technology conferences. The Sixth Annual Clean Coal Technology Conference was held in Reno, Nevada from April 28 to May 1, 1998. The conference focused on "What will it take?" to realize the full commercial potential of clean coal technologies.

Panel discussions at the conference identified two basic issues that currently drive future technology decisions in the domestic market—environmental concerns and utility restructuring. With regard to environmental concerns, the CCT Program has provided a portfolio of technologies to effectively deal with acid rain concerns. Challenges remain, however, in achieving ozone standards (a NO_x control issue), $PM_{2.5}$ control, and CO_2 emission reductions. With regard to utility restructuring, some 40 percent of the states are sponsoring conceptually and functionally different legislation driven by different rate structures, fuel mixes, stranded cost implications, and environmental policies. Thus, some argue that federal legislation is needed to provide some consistency in what might otherwise become an unnavigable maze of implementing mechanisms. Whatever the outcome of restructuring, it will have an impact–positive or negative–on the future of clean coal technologies.

An International Business Forum was held at the conference to identify emerging opportunities for clean coal technologies worldwide. The consensus is that the international market for clean coal technologies has tremendous near-term potential. To capitalize on this market potential requires action to mitigate the higher

Exhibit ES-5
Commercial Successes—Advanced Electric Power Generation

Project and Participant	Commercialization Progress
Tidd PFBC Demonstration Project (The Ohio Power Company)	First utility-scale PFBC in U.S. – Laid foundation for commercialization of PFBC The first 360-MWe ABB Carbon P800 PFBC plant is being built in Japan A second generation ABB Carbon P200 PFBC is under construction in Germany Other ABB Carbon PFBC projects are under consideration in China, South Korea, the United Kingdom, Italy, and Israel
Nucla CFB Demonstration Project (Tri-State Generation and Transmission Association, Inc.)	Technology retained for commercial use at host site – World's first large utility-scale ACFB Demonstration commercialized utility-scale ACFB – Quantity—29 CFB units larger than 100-MWe planned, in construction, or in operation worldwide – Estimated capacity—greater than 6,200 MWe – Estimated value—almost $6 billion
Tampa Electric Integrated Gasification Combined-Cycle Project (Tampa Electric Company)	First greenfield IGCC unit in commercial service Texaco, Inc., and ASEA Brown Boveri signed an agreement forming an alliance to market IGCC technology in Europe
Wabash River Coal Gasification Repowering Project (Wabash River Coal Gasification Repowering Project Joint Venture)	First repowered IGCC unit in commercial service – World's largest single train IGCC in commercial service – Preferentially dispatched over other coal-fired units in PSI Energy's system because of high efficiency
Piñon Pine IGCC Power Project (Sierra Pacific Power Company)	Unit in operation
Healy Clean Coal Project (Alaska Industrial Development and Export Authority)	TRW offering licensing of combustor worldwide (China agreement in place)

risk and cost of clean coal technologies. Trading mechanisms for CO_2 such as the 161-nation "Global Environmental Facility" and others proposed under the Kyoto Protocol hold promise for reducing the incremental costs for clean coal technologies, assuming CO_2 reduction requirements or incentives are formalized. Fluidized-bed combustion and IGCC technologies have begun to penetrate the market.

In addition to the Sixth Annual Clean Coal Technology Conference, several other conferences and workshops were held in fiscal year 1998. The forums for the conferences varied from China to West Virginia to Ukraine. Trade missions during fiscal year 1998 included China, Korea, Uruguay, Brazil, Japan, and the Philippines. All of these conferences and trade missions were used to endorse and promote the technologies demonstrated in the CCT Program.

CCT Projects

Technology Overview. The 40 CCT Program projects provide a portfolio of technologies that will enable coal to continue to provide low-cost secure energy vital to the nation's economy while satisfying energy and environmental goals well into the 21st century.

Exhibit ES-6
Summary of Results of Coal Processing for Clean Fuels

Project and Participant	Key Results	Capital Cost
Development of the Coal Quality Expert™ (ABB Combustion Engineering, Inc., and CQ Inc.)	CQE™ features: Fuel evaluator—performs system-, plant-, and/or unit-level fuel quality, economic, and technical assessments Plant engineer—provides in-depth performance evaluations with a more focused scope than provided in the fuel evaluator Environmental planner—provides access to evaluation and presentation capabilities of the Acid Rain Advisor Coal cleaning expert—establishes the feasibility of cleaning a coal, determines cleaning processes, and predicts associated costs	CQE™ package sells for between $75,000 and $100,000
ENCOAL® Mild Gasification Project (ENCOAL Corporation)	The liquid (CDL®) and solid (PDF®) product fuels have been used economically in commercial boilers and furnaces and have reduced SO_2 and NO_x emissions significantly at utility and industrial facilities currently burning high-sulfur bituminous coal or fuel oils Almost five years of operating data have been collected for use as a basis for the evaluation and design of a commercial plant As of July 1997, about 260,000 tons of coal had been processed into 120,000 tons of PDF® and 5,101,000 gallons of CDL®	A commercial plant designed to process 15,000-metric-ton/day would cost $475 million (2001$) to construct with annual operating and maintenance costs of $52 million per year

Environmental Control Devices. The environmental control technologies provide a suite of cost-effective control options for the full range of boiler types. The 19 environmental control device projects are valued at more than $704 million. These include seven NO_x emission control systems installed in more than 1,750 MWe of utility generating capacity, five SO_2 emissions systems installed on approximately 770 MWe, and seven combined SO_2/NO_x emission control systems installed or planned for installation on more than 665 MWe of capacity.

Advanced Electric Power Generation. To respond to load growth, as well as growing environmental concerns, the CCT Program provides a range of advanced electric power generation options for both repowering and new power generation. These advanced options offer greater than 20 percent reductions in greenhouse gas emissions; SO_2, NO_x, and particulate emissions far below NSPS; and salable solid and liquid by-products in lieu of solid wastes. Over 1,800 MWe of capacity are represented by 11 projects valued at more than $3.1 billion. These projects will not only provide environmentally sound electric generation in the mid- to late-1990s, but also will provide the demonstrated technology base necessary to meet new capacity requirements in the 21st century.

Exhibit ES-7
Commercial Successes—Coal Processing for Clean Fuels

Project and Participant	Commercialization Progress
Development of the Coal Quality Expert™ (ABB Combustion Engineering, Inc. and CQ Inc.)	CQ Inc. and Black & Veatch working collaboratively to commercialize CQE™ worldwide CQE's Acid Rain Advisor licensed to two U.S. users 30 U.S. and 1 U.K. utilities acquired CQE™ through EPRI membership Other foreign and domestic utilities pursuing access to CQE™ CQE technology saves U.S. utilities $26 million CQE™ Home Page posted on World Wide Web (http://www.fuels.bv.com:80/cqe/cqe.htm)
Self-Scrubbing Coal™: An Integrated Approach to Clean Air (Custom Coals International)	Proposed agreement to purchase 1 million tons/yr in U.S. Proposed agreement with China to build a coal-cleaning plant, slurry pipeline, and port facility – Value—$450 million Letter of intent for three additional pipelines in China – Value—$3 billion Letters of intent from Polish utilities for 5 million tons/yr – Value—$50 million
Advanced Coal Conversion Process Demonstration (Rosebud SynCoal Partnership)	Total sales of SynCoal® product exceeds 1,400,000 tons Agreement in place to provide SynCoal® to fuel Montana Power's 330 MWe Colstrip No. 2 A commercial project being developed – Stand-alone minemouth design in Wyoming
ENCOAL® Mild Gasification Project (ENCOAL Corporation)	Over 83,500 tons of solid fuel delivered to seven major utilities and metallurgical customers Over 200 tank cars of liquid fuel delivered to eight industrial users Permitting of a 15,000 metric-ton/day commercial plant in Wyoming is nearly complete – Value—$460 million Completed five feasibility studies—two Indonesian, one Russian, and two U.S. projects
Commercial-Scale Demonstration of the Liquid-Phase Methanol (LPMEOH™) Process (Air Products Liquid-Phase Conversion Company, L.P.)	Nominal 80,000 gallon/day methanol production being used by Eastman Chemical Company

Coal Processing for Clean Fuels. Also addressed are approaches to converting run-of-mine coals to high-energy-density, low-sulfur products. These products have application domestically for compliance with the CAAA. Internationally, both the products and processes have excellent market potential. Valued at more than $51 million, the five projects in the coal processing for clean fuels category represent a diversified portfolio of technologies.

Industrial Processes. Projects were undertaken as well to address pollution problems associated with coal use in the industrial sector. The problems addressed include dependence of the steel industry on coke and the inherent pollutant emissions in coke-making; reliance of the cement industry on low-cost indigenous, and often high-sulfur, coal fuels; and the need for many industrial boiler operators to consider switching to coal fuels to reduce operating costs. The five industrial applications projects have a combined value of nearly $1.3 billion. The projects encompass substitution of coal for 40 percent of coke in iron-making, integration of a direct iron-making process with the production of electricity; reduction of cement kiln emissions and solid waste generation; demonstration of an industrial-scale slagging combustor; and demonstration of a pulse combustor system.

Project Fact Sheets. The core of this *Program Update 1998* is the project fact sheets. Two types of fact sheets are provided: (1) a brief two-page overview

Exhibit ES-8
Summary of Results of Industrial Application Projects

Project and Participant	Key Results	Capital Cost
Advanced Cyclone Combustor with Internal Sulfur, Nitrogen, and Ash Control (Coal Tech Corporation)	SO_2 reduction of over 80% with sorbent injection; 58% maximum with limestone injection at 2.0 Ca/S molar ratio NO_x emissions of 160–184 ppm (75% reduction) Slag/sorbent retention of 55–90% in combustor; inert slag	Not available
Cement Kiln Flue Gas Recovery Scrubber (Passamaquoddy Tribe)	SO_2 reduction of 90–95% (2.5–3% sulfur bituminous coal); 98% maximum reduction NO_x reduction of 18.8% avg Particulate emissions of 0.005–0.007 gr/std ft^3 with loading of 0.04 gr/std ft^3	$10 million for 450,000 ton/yr wet-process plant (1990$)

for ongoing projects or (2) an expanded four-page summary for projects that have successfully completed operational testing. The latter contain a summary of the major results from the demonstrations, as well as sources for obtaining further information. Technology descriptions, costs, and schedules are provided for all projects. A list of the project fact sheets with the participant, solicitation, and status is shown in Exhibit ES-10. A list of the award winning CCT Program projects is shown in Exhibit ES-11.

Exhibit ES-9
Commercial Successes—Industrial Applications

Project and Participant	Commercialization Progress
Blast Furnace Granular-Coal Injection System Demonstration Project (Bethlehem Steel Corporation)	British Steel granted exclusive marketing rights to technology co-developer, CPC-Macawber Commercial sale of technology to United States Steel Corporation
Cement Kiln Flue Gas Recovery Scrubber (Passamaquoddy Tribe)	Technology retained for commercial use at host site Completed feasibility study for Taiwanese cement plant

Exhibit ES-10
Projects by Application Category

Project	Participant	Solicitation/Status
Environmental Control Devices		
SO_2 Control Technologies		
10-MWe Demonstration of Gas Suspension Absorption	AirPol, Inc.	CCT-III/completed 3/94
Confined Zone Dispersion Flue Gas Desulfurization Demonstration	Bechtel Corporation	CCT-III/completed 6/93
LIFAC Sorbent Injection Desulfurization Demonstration Project	LIFAC–North America	CCT-III/completed 6/94
Advanced Flue Gas Desulfurization Demonstration Project	Pure Air on the Lake, L.P.	CCT-II/completed 6/95
Demonstration of Innovative Applications of Technology for the CT-121 FGD Process	Southern Company Services, Inc.	CCT-II/completed 12/94
NO_x Control Technologies		
Micronized Coal Reburning Demonstration for NO_x Control	New York State Electric & Gas Corporation	CCT-IV/operational
Demonstration of Coal Reburning for Cyclone Boiler NO_x Control	The Babcock & Wilcox Company	CCT-II/completed 12/92
Full-Scale Demonstration of Low-NO_x Cell Burner Retrofit	The Babcock & Wilcox Company	CCT-III/completed 4/93
Evaluation of Gas Reburning and Low-NO_x Burners on a Wall-Fired Boiler	Energy and Environmental Research Corporation	CCT-III/completed 1/95
Demonstration of Selective Catalytic Reduction Technology for the Control of NO_x Emissions from High-Sulfur-Coal-Fired Boilers	Southern Company Services, Inc.	CCT-II/completed 7/95
180-MWe Demonstration of Advanced Tangentially Fired Combustion Techniques for the Reduction of NO_x Emissions from Coal-Fired Boilers	Southern Company Services, Inc.	CCT-II/completed 12/92
Demonstration of Advanced Combustion Techniques for a Wall-Fired Boiler	Southern Company Services, Inc.	CCT-II/completed 5/98
Combined SO_2/NO_x Control Technologies		
Commercial Demonstration of the NOXSO SO_2/NO_x Removal Flue Gas Cleanup System	NOXSO Corporation	CCT-III/design
SNOX™ Flue Gas Cleaning Demonstration Project	ABB Environmental Systems	CCT-II/completed 12/94
LIMB Demonstration Project Extension and Coolside Demonstration	The Babcock & Wilcox Company	CCT-I/completed 8/91
SO_x-NO_x-Rox Box™ Flue Gas Cleanup Demonstration Project	The Babcock & Wilcox Company	CCT-II/completed 5/93
Enhancing the Use of Coals by Gas Reburning and Sorbent Injection	Energy and Environmental Research Corporation	CCT-I/completed 10/94
Milliken Clean Coal Technology Demonstration Project	New York State Electric & Gas Corporation	CCT-IV/completed 6/98
Integrated Dry NO_x/SO_2 Emissions Control System	Public Service Company of Colorado	CCT-III/completed 12/96
Advanced Electric Power Generation		
Fluidized-Bed Combustion		
McIntosh Unit 4A PCFB Demonstration Project	City of Lakeland, Lakeland Electric	CCT-III/design
McIntosh Unit 4B Topped PCFB Demonstration Project	City of Lakeland, Lakeland Electric	CCT-V/design
JEA Large Scale CFB Combustion Demonstration Project	JEA	CCT-I/design

Shaded area indicates projects having completed operations.

Exhibit ES-10 (continued)
Projects by Application Category

Project	Participant	Solicitation/Status
Tidd PFBC Demonstration Project	The Ohio Power Company	CCT-I/completed 3/95
Nucla CFB Demonstration Project	Tri-State Generation and Transmission Association, Inc.	CCT-I/completed 1/91
Integrated Gasification Combined Cycle		
Clean Energy Demonstration Project	Clean Energy Partners Limited Partnership	CCT-V/design
Piñon Pine IGCC Power Project	Sierra Pacific Power Company	CCT-IV/operational
Tampa Electric Integrated Gasification Combined-Cycle Project	Tampa Electric Company	CCT-III/operational
Wabash River Coal Gasification Repowering Project	Wabash River Coal Gasification Repowering Project Joint Venture	CCT-IV/operational
Advanced Combustion/Heat Engines		
Healy Clean Coal Project	Alaska Industrial Development and Export Authority	CCT-III/operational
Clean Coal Diesel Demonstration Project	Arthur D. Little, Inc.	CCT-V/construction
Coal Processing for Clean Fuels		
Commercial-Scale Demonstration of the Liquid-Phase Methanol (LPMEOH™) Process	Air Products Liquid-Phase Conversion Company, L.P.	CCT-III/operational
Self-Scrubbing Coal™: An Integrated Approach to Clean Air	Custom Coals International	CCT-IV/design
Advanced Coal Conversion Process Demonstration	Rosebud SynCoal Partnership	CCT-I/operational
Development of the Coal Quality Expert™	ABB Combustion Engineering, Inc., and CQ Inc.	CCT-I/completed 12/95
ENCOAL Mild Coal Gasification Project	ENCOAL Corporation	CCT-III/completed 7/97
Industrial Applications		
Blast Furnace Granular-Coal Injection System Demonstration Project	Bethlehem Steel Corporation	CCT-III/operational
Clean Power from Integrated Coal/Ore Reduction (CPICOR™)	CPICOR™ Management Company, L.L.C.	CCT-V/design
Pulse Combustor Design Qualification Test	ThermoChem, Inc.	CCT-IV/design
Advanced Cyclone Combustor with Internal Sulfur, Nitrogen, and Ash Control	Coal Tech Corporation	CCT-I/completed 5/90
Cement Kiln Flue Gas Recovery Scrubber	Passamaquoddy Tribe	CCT-II/completed 9/93

Shaded area indicates projects having completed operations.

Exhibit ES-11
Award-Winning CCT Projects

Project and Participant	Award
Full-Scale Demonstration of Low-NO_x Cell Burner Retrofit (The Babcock & Wilcox Company)	1994 R&D 100 Award presented by *R&D* magazine to the U.S. Department of Energy for development of the low-NO_x cell burner.
Evaluation of Gas Reburning and Low-NO_x Burners on a Wall-Fired Boiler; Enhancing the Use of Coals by Gas Reburning and Sorbent Injection (Energy and Environmental Research Corporation)	1997 J. Deanne Sensenbaugh Award presented by the Air and Waste Management Association to the U.S. Department of Energy, Gas Research Institute, and U.S. Environmental Protection Agency for the development and commercialization of gas-reburning technology.
Advanced Flue Gas Desulfurization Demonstration Project (Pure Air on the Lake, L.P.)	1993 Powerplant Award presented by *Power* magazine to Northern Indiana Public Service Company's Bailly Generating Station.
	1992 Outstanding Engineering Achievement Award presented by the National Society of Professional Engineers.
Demonstration of Innovative Applications of Technology for the CT-121 FGD Process (Southern Company Services, Inc.)	1995 Design Award presented by the Society of Plastics Industries in recognition of the mist eliminator.
	1994 Powerplant Award presented by *Power* magazine to Georgia Power's Plant Yates. Co-recipient was the U.S. Department of Energy.
	1994 Outstanding Achievement Award presented by the Georgia Chapter of the Air and Waste Management Association.
	1993 Environmental Award presented by the Georgia Chamber of Commerce.
Tidd PFBC Demonstration Project (The Ohio Power Company)	1992 National Energy Resource Organization award for demonstration of energy-efficient technology.
	1991 Powerplant Award presented by *Power* magazine to American Electric Power Company's Tidd project. Co-recipient was The Babcock & Wilcox Company.
Tampa Electric Integrated Gasification Combined-Cycle Project (Tampa Electric Company)	1997 Powerplant Award presented by *Power* magazine to Tampa Electric's Polk Power Station.
	1996 Association of Builders and Contractors Award presented to Tampa Electric for quality of construction.
	1993 Ecological Society of America Corporate Award presented to Tampa Electric for its innovative siting process.
	1993 Timer Powers Conflict Resolution Award presented to Tampa Electric by the state of Florida for the innovative siting process.
	1991 Florida Audubon Society Corporate Award presented to Tampa Electric for the innovative siting process.
Wabash River Coal Gasification Repowering Project (Wabash River Coal Gasification Repowering Project Joint Venture)	1996 Powerplant Award presented by *Power* magazine to CINergy Corp./PSI Energy, Inc.
	1996 Engineering Excellence Award presented to Sargent & Lundy upon winning the 1996 American Consulting Engineers Council competition.
Development of the Coal Quality Expert™ (ABB Combustion Engineering, Inc. and CQ Inc.)	In 1996 recognized by then Secretary of Energy Hazel O'Leary and EPRI President Richard Balzhiser as the best of nine DOE/EPRI cost-shared utility R&D projects under the Sustainable Electric Partnership Program.

1. Role of the CCT Program

Introduction

Over the past quarter century, the nation's energy picture has been one of dynamic change. The nation's energy policy has responded to the oil embargoes of the 1970s and the environmental debates of the 1980s. The 1990s have brought about more changes in response to required emission reductions for acid rain precursors, initiation of more stringent NO_x standards for ozone nonattainment areas, the beginning of electric utility restructuring, and concern about global warming. These changes have also reshaped the private sector's response in the domestic and international marketplace.

Since 1985, a joint effort between government and industry, known as the Clean Coal Technology Demonstration Program (CCT Program), has responded to the challenges resulting from these dynamic changes. The magnitude of the projects and extent of industry participation in the CCT Program is unprecedented. More than $5.6 billion is being expended, with industry and state governments investing two dollars for every federal government dollar invested. With 57 percent of the projects having completed operations by the end of fiscal year 1998, the technological successes have manifested themselves in the marketplace. New technologies to reduce the emissions of acid rain precursors, namely sulfur dioxide (SO_2) and nitrogen oxides (NO_x), are now in the marketplace and are being used by electric power producers and heavy industry. Advanced electric power generation systems that generate electricity with greater efficiency and fewer environmental consequences are now operating with the nation's most plentiful fossil energy resource—coal. Coal, which accounts for over 94 percent of the proven fossil energy reserves in the United States, supplies the bulk of the low-cost reliable electricity vital to the nation's economy and global competitiveness. According to the U.S. Department of Energy's (DOE) Energy Information Administration (EIA), coal was used to produce over 1,797 billion kilowatt-hours or 52 percent of the nation's electricity in 1996. EIA projections count on coal continuing to dominate electric power production, at least through 2020 (the end of the forecast period), when coal will generate an estimated 2,304 billion kilowatt-hours or nearly 49 percent of all electricity generated.

The ability of coal and coal technologies to respond to the nation's need for low-cost reliable electricity hinges on the ability to meet two central requirements: (1) environmental performance requirements established in current and emerging laws and regulations and (2) operational and economic performance requirements to compete in the era of utility restructuring and competition. The CCT Program is responding to these requirements by producing a portfolio of advanced coal-based technologies that will enable coal to retain its prominent role in the nation's power generation future. Furthermore, advanced technologies emerging from the CCT Program will also enhance coal's competitive position in the industrial sector. For example, technology advances in steelmaking, involving direct use of coal, will reduce the cost of production while greatly improving environmental performance. Coal could increase its market share in the industrial sector through cogeneration (steam and electricity) and coproduction of products (clean fuels and chemicals).

While the CCT Program responds to domestic needs for competitive and clean coal-based technology, it also positions U.S. industry to compete in a burgeoning power market abroad. Coal is the fuel of necessity for many foreign economies. Through the CCT Program, U.S. industry has obtained the knowledge base needed to replicate clean coal technologies both domestically and abroad.

Coal Technologies Respond to Need

The environmental and competitive performance of modern coal technologies has evolved through many years of industry and government research, development, and demonstration (RD&D). The programs were pursued to assure that the U.S. recoverable coal reserves of 274 billion tons, which represent a secure energy source, could supply the nation's energy needs economically and in an environmentally acceptable manner.

During the 1970s and early 1980s, many of the government-sponsored technology demonstrations focused on synthetic fuels production technology. Under the Energy Security Act of 1980, the Synthetic Fuels Corporation (SFC) was established for the purpose of reducing the U.S. vulnerability to disruptions of crude oil imports. The SFC's purpose was accomplished by encouraging the private sector to build and operate synthetic fuel production facilities that would use abundant domestic energy resources, primarily coal and oil shale. The strategy was for the SFC to be primarily a financier of pioneer commercial and near-commercial scale facilities.

The goal of the SFC was to achieve production capacities of 500,000 barrels per day of synthetic fuels by 1987 and 2 million barrels per day by 1992, at an estimated cost of $8.8 billion. By 1985, it became apparent that the need for synthetic fuels had changed, as oil prices declined, world oil supplies stabilized, and a short-term supply buffer was provided by the Strategic Petroleum Reserve. In 1986, Congress responded to the decline of private-sector interest in the production of synthetic fuels in light of these market conditions. Public Law 99-190, Department of the Interior and Related Agencies Appropriations Act for Fiscal Year 1986, abolished the SFC and transferred project management to the Treasury Department.

The CCT Program was initiated in October, 1984. Public Law 98-473, Joint Resolution Making Continuing Appropriation for Fiscal Year 1985 and Other Purposes, provided $750 million from the Energy Security Reserve to be deposited in a separate account in the U.S. Treasury entitled The Clean Coal Technology Reserve. The nation moved from an energy policy based on synthetic fuels production to a more balanced policy, which established that the nation should have an adequate supply of energy; maintained at a reasonable cost; and consistent with environmental, health, and safety objectives. Energy stability, security, and strength were the foundations for this policy. Coal was recognized as an essential element in this energy policy for the foreseeable future because of the following:

1. The location, magnitude, and characteristics of the coal resource base are well understood.

2. The technology and skilled labor base to safely and economically extract, transport, and use coal are available.

3. A multi-billion dollar infrastructure is in place to gather, transport, and deliver this valuable energy commodity to serve the domestic and international marketplace.

4. Coal is used to produce over half of the nation's electric power and is vital to industrial processes, such as steel and cement production, as well as industrial power.

5. This abundant fossil energy resource is secure within the nation's borders and relatively invulnerable to disruptions because of the coal industry's production responsiveness and stockpiling capability.

6. Coal is the fuel of necessity in many lesser developed economies, which provides export opportunities for U.S. developed coal-based technologies.

Congress recognized that the continued viability of coal as a source of energy was dependent on the demonstration and commercial application of a new generation of advanced coal-based technologies characterized by enhanced operational, economic, and environmental performance. The CCT Program was established to demonstrate the commercial feasibility of clean coal technology applications in response to that need. In 1986, the first solicitation (CCT-I) for clean coal technology projects was issued. The CCT-I solicitation resulted in a broad range of projects being selected in four major product markets—environmental control devices, advanced electric power generation, coal processing for clean fuels, and industrial applications.

In 1987, the CCT Program became the centerpiece for satisfying the recommendations contained in the *Joint Report of the Special Envoys on Acid Rain* (1986). A presidential initiative launched a five-year, $5-billion U.S. industry/government effort to curb precursors of acid rain formation—SO_2 and NO_x. Thus, the second solicitation (CCT-II) issued in February 1988, provided for the demonstration of technologies that were capable of achieving significant emission reductions in SO_2, NO_x, or both, from existing power plants. These technologies were to be more cost-effective than current technologies and capable of commercial deployment in the 1990s. In May 1989, a third solicitation (CCT-III) was issued with essentially the same objective as the second, but additionally encouraged technologies that would produce clean fuels from run-of-mine coal.

The next two solicitations recognized emerging energy and environmental issues, such as global climate change and capping of SO_2 emissions, and thus focused on seeking highly efficient, economically competitive, and low-emission technologies. Specifically, the fourth solicitation (CCT-IV), released in January 1991, had as its objective the demonstration of energy efficient, economically competitive technologies capable of retrofitting, repowering, or replacing existing facilities while achieving significant reductions in SO_2 and NO_x emissions. In July 1992, the fifth and final solicitation (CCT-V) was issued to provide for demonstration projects that significantly advanced the efficiency and environmental performance of technologies applicable to new or existing facilities. As a result of these five solicitations, a total of 60 government/industry cost-shared projects were selected, of which 40 valued at more than $5.6 billion have either been successfully completed or remain active in the CCT Program.

The success of the government/industry CCT Program is directly attributable to the CCT Program's responsiveness to public and private sector needs to reduce environmental emissions and maximize economic and efficient energy production. The CCT Program will strengthen the economy, enhance energy security, and reduce the vulnerability of the economy to global energy market shocks.

Coal Technologies for Environmental Performance

Acid Rain Mitigation

SO_2 Control. During the late 1980s, work began on drafting what was to become the CAAA. On November 15, 1990, Congress enacted Public Law 101-549, the Clean Air Act Amendments of 1990. Title IV, Acid Deposition Control, established emissions reduction targets for SO_2, capped SO_2 emission in the post-2000 timeframe, and directed the establishment of allowable emission limitations for NO_x. Title IV represented the first large-scale approach to regulating overall emissions levels by using marketable allowances. The utilities could adopt a control strategy that was most cost-effective for their given systems and plants rather than having to apply a "command-and-control" approach wherein the emission-reduction method is specified.

The emission reduction requirements for SO_2 were to be met in two phases. Phase I, which provided for the initial increment of SO_2 reduction, began on January 1, 1995. The second increment implemented through Phase II will begin on January 1, 2000. Title IV identified 261 generating units (designated as "affected units") that were required to comply with Phase I. Most of these units are coal-fired with fairly high emission rates. Exhibit 1-1 summarizes the compliance methods used by the 261 affected units listed in Title IV to satisfy Phase I requirements. An additional 174 units are participating in Phase I based on U.S. Environmental Protection Agency (EPA) rules that allow a utility to designate substitution or compensating units as part of Phase I compliance strategies. Therefore, 435 units are considered Phase I units. Under Phase II, more than 2,000 units will be affected.

By the end of 1995, the Phase I units had significantly reduced SO_2 emissions compared to previous years. In 1990, the Phase I units emitted 9.7 million tons of SO_2, in 1995 emissions were down to 5.3 million tons, a 45 percent reduction. On the other hand, non-Phase I unit emissions were 12 percent higher (6.6 million tons) than their 1990 emissions of 5.9 million tons.

Several projects within the CCT Program, listed below, were designated affected units and were required to achieve compliance with Phase I requirements:

- Northern Indiana Public Services Company's Bailly Generating Station, 528-MWe Unit Nos. 7 and 8 (Pure Air advanced flue gas desulfurization scrubber);
- Georgia Power Company's Plant Yates, 100-MWe Unit No. 1 (Chiyoda Thoroughbred-121 advanced flue gas desulfurization scrubber);

Exhibit 1-1
Phase I SO_2 Compliance Methods

Method	No. of Units	% of Units	% SO_2 Reduction from 1985 Baseline	% of Total SO_2 Reduction
Fuel switching/blending	136	52	60	59
Additional SO_2 allowances	83	32	16	9[a]
Scrubbers	27	10	83	28
Retirements	7	3	100	2
Other[b]	8	3	86	2
Total	261	100	345	100

[a] Includes reduced coal consumption of 2.5 million tons and 16% reduction in sulfur content.
[b] Includes 1 repowered unit, 2 switched to natural gas, and 5 switched to No. 6 fuel oil.
Source: *The Effects of Title IV of the Clean Air Act Amendments of 1990 on Electric Utilities: An Update*, Energy Information Administration, March 1997.

- New York State Electric & Gas Corporation's Milliken Station, 300-MWe Unit Nos. 1 and 2 (S-H-U formic-acid-enhanced wet limestone scrubber); and
- PSI Energy's Wabash River Station, 262-MWe Unit No. 1 (repowered with Destec integrated gasification combined-cycle unit).

One of the more significant effects of compliance with Phase I requirements was the change in coal use. As shown in Exhibit 1-1, the fuel switching/blending compliance strategy was selected for 52 percent of the affected units. This switch to lower sulfur coal affected regional coal distribution. Between 1990 and 1995, the following changes in coal sales resulted:

- Powder River Basin coal—increased 78 million tons,
- Central Appalachian coal—increased 15 million tons,
- Rocky Mountain coal—increased 10 million tons,
- Northern Appalachian coal—decreased 29 million tons, and
- Illinois Basin coal—decreased 40 million tons.

In Phase II, beginning January 1, 2000, annual SO_2 tonnage emission limitations will be determined based on a 1.20 lb/10^6 Btu emission rate and 1985-87 baseline fuel consumption. Most utilities have still not finalized their compliance strategies because the industry is faced with major changes in the way it is structured and does business under the requirements of the Federal Energy Regulatory Commission (FERC) Order Nos. 888 and 889 and state-level utility restructuring legislation. Under the previous regulatory environment, state regulators would allow utilities to pass on pollution control costs to consumers. In a restructured competitive environment, the added cost of capital-intensive environmental controls could put a utility at a disadvantage relative to those utilities that can achieve compliance with lower cost alternatives, such as fuel switching and blending. The EIA projects that fuel switching and blending will be the predominant strategy used, with emission allowance purchases being the second choice. However, allowance prices are increasing and are expected to increase significantly after 2000, making the scrubbing option more cost competitive. The EIA projects that by 2010 about 23 gigawatts of coal-fired capacity will be retrofitted with scrubbers. The technologies applied will have their roots in the CCT Program, which redefined the state-of-the-technology in scrubbers and essentially halved the cost relative to conventional scrubbers of the time. Another option available to utilities is to repower with a clean coal technology. Under the repowering option, a four-year extension (to December 31, 2003) is available to comply with the Phase II requirements with advanced electric power generation technology.

▲ New York State Electric & Gas Corporation's Milliken Station used the S-H-U scrubber to achieve 98 percent SO_2 removal and compliance with Phases I & II of the CAAA.

NO_x Control. In Title IV of the CAAA, Congress also required the EPA to establish annual allowable emissions limitations for NO_x in two phases. Phase I required NO_x reductions from tangentially-fired and dry-bottom wall-fired boilers. These boilers are referred to as Group 1 boilers. In March 1994, EPA promulgated a rule establishing NO_x emission limitations of 0.45 lb/10^6 Btu for tangentially-fired units and 0.50 lb/10^6 Btu for wall-fired units. However, in November 1994 after a challenge from utility groups, the U.S. Court of Appeals found that the definition of low-NO_x burner technology contained in the March rule exceeded EPA's statutory authority and vacated the rule. In April 1995, after agreement with environmental and utility organizations, EPA issued a final rule revising the definition of low-NO_x burner technology. Furthermore, the rule extended the compliance date to January 1, 1996.

On August 3, 1995, EPA issued a proposed regulation that included a provision for "open market" trading, somewhat similar to SO_2 allowance trading. Under this rule, utilities would not need federal and state approval for transactions of NO_x and volatile organic compounds (VOCs) credit trading. Instead, utilities would be able to comply with various air pollution mandates by buying and using an appropriate number of tons of “discrete emissions reductions” (DERs). Utilities would be able to generate emission reduction credits for smog precursors by voluntarily reducing NO_x and VOCs and then bank, use, or sell the credits under the open market emissions trading proposal. (In addition to trading VOCs and NO_x under the program, the utilities also would be able to trade water pollution credits.) The DERs will not require certification by regulators until they are used, either by the utility that generates them for later use or by a second utility that purchases the DERs from the first utility.

On December 19, 1996, EPA issued a rule to implement Phase II. The rule established NO_x emission limitations for additional coal-fired boilers (Group 2) and reduced the NO_x emissions limitations on Group 1 boilers. The types of Group 1 and 2 boilers and the Phase I and II NO_x emission limits are shown in Exhibit 1-2.

Exhibit 1-2
CAAA NO_x Emission Limits

Group 1 Boiler Type	Group 2 Boiler Type	Phase I NO_x Emission Limits[a] ($lb/10^6$ Btu)	Phase II NO_x Emission Limits[a] ($lb/10^6$ Btu)
Tangentially-fired boilers		0.45	0.40
Dry-bottom wall-fired boilers[b]		0.50	0.46
	Cell-burner boilers		0.68
	Cyclone boilers >155 MWe		0.86
	Wet-bottom wall-fired boilers >65 MWe		0.84
	Vertically fired boilers		0.80

[a] Emission limits are $lb/10^6$ Btu of heat input on an annual average basis.
[b] Other than units applying cell-burner technology.

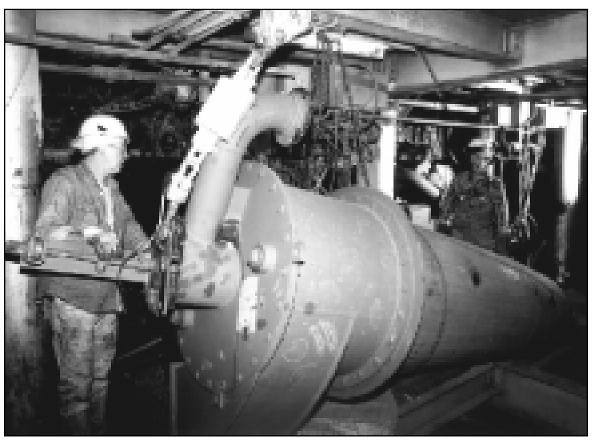
In response to the need to formulate NO_x emission reductions that were realistic and achievable for Group 1, EPA was able to use data developed during the Southern Company Services’ evaluation of NO_x control on wall-fired and tangentially-fired boilers. Furthermore, operational, environmental, and economic data on NO_x controls were developed under the CCT Program for all four major boiler types (wall-fired, tangentially-fired, cyclone-fired, and cell-burner), which constitute over 90 percent of the pre-New Source Performance Standard (NSPS) boiler types. In addition, low-NO_x burners were installed and tested on a vertically-fired boiler. Other alternative NO_x control technologies were demonstrated, including coal and gas reburning, selective noncatalytic reduction (SNCR), and selective catalytic reduction (SCR). This portfolio of NO_x controls will not only assure Phase I and II emission reductions are achievable, but will provide the technology base necessary to achieve even deeper NO_x reductions that may be necessary to meet CAAA Title I requirements or new National Ambient Air Quality Standards (NAAQS) for ozone.

▲ Chiyoda’s CT-121 system demonstrated at Georgia Power’s Plant Yates achieved high SO_2 capture efficiencies and enhanced capture of particulate matter.

New Rules

The EPA is in the process of considering and issuing new rules that go beyond the acid rain provisions contained in the CAAA. Some of these rules are in the discussion phase; other rules have been proposed or finalized and will need to be considered in the research, development, and deployment of clean coal technologies. The following rules are illustrative.

Attainment of Ozone Standards (Title I). CAAA Title I established an ozone transport commission to address regional transport of pollutants that contribute to ozone nonattainment in the Northeast. The Northeast Ozone Transport Commission approved a Memorandum of Understanding in September 1994 stipulating intent to reduce power plant emissions of NO_x (a precursor to ozone formation) by as much as 70 percent by 2003. The Ozone Transport Assessment Group (OTAG), a collaborative effort by 37 states and the District of Columbia, was established in June 1995 to address the issue of ozone transportation. In response to recommendations issued in June 1997 by the OTAG Policy Group, EPA issued a "SIP Call" to 22 states and the District of Columbia. The SIP Call (effective December 28, 1998, as EPA's ozone-transport rule) requires these 23 jurisdictions to submit emission reduction plans by December 30, 1999 on how to cut NO_x emissions 85 percent below 1990 rates or achieve a 0.15 lb/10^6 Btu emission rate by May 2003.



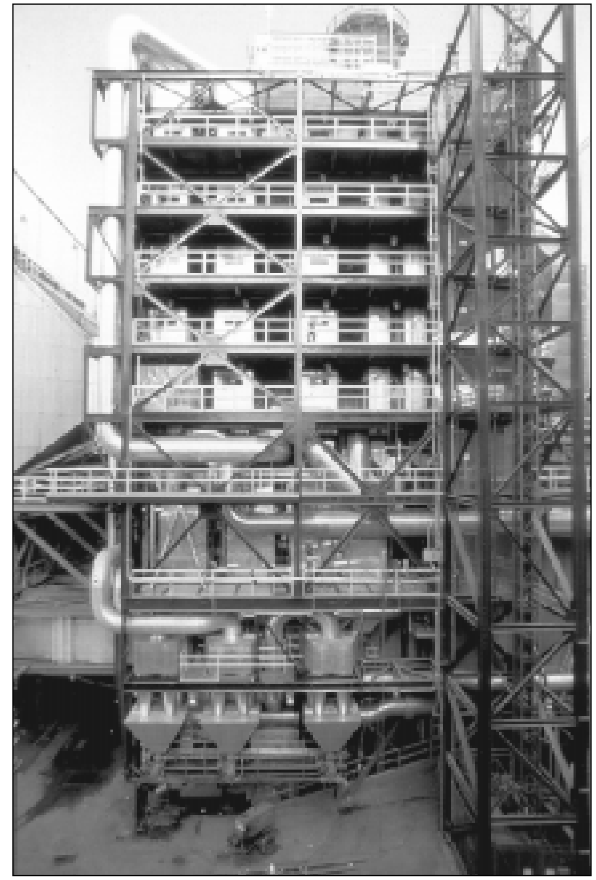
▲ NO_x emissions at Georgia Power's Plant Hammond were reduced by 63 percent with Foster Wheeler's low-NO_x burners, shown here, and advanced overfire air.

The EPA is also formulating a plan for utilities and industries to trade allowances for NO_x emissions. The "cap and trade" program would apply to the 23 jurisdictions affected by the SIP Call. The EPA states that most areas will be able to meet air quality standards without additional air controls. Under the plan, the affected jurisdictions would establish a cap on NO_x emissions and then give power plants and industries the flexibility to cut NO_x emissions in the most cost-effective manner. Power plants and industries that cut NO_x emissions below the caps could sell credits to facilities that could not cut emissions as quickly or cost-effectively.

The NO_x trading program, similar to the SO_2 trading program, allows sources to pursue various compliance strategies; such as fuel switching; installing pollution control devices, like the devices demonstrated in the CCT Program; or buying allowances from sources that over-complied.

The EPA has tightened its NO_x emission standards for new electric utility boilers and has changed its rules so that all generation fuels are treated equally. Under the revised new source performance standard, electric utility and industrial steam generating units built or modified after July 9, 1997, must meet an emission limit of 1.6 lb/MWh regardless of fuel type. For existing sources that become subject to new standards, the NO_x limit is now 0.15 lb/10^6 Btu. By basing the standard on electricity output, there is an economic incentive to use more efficient systems.

Soot and Smog. In 1997, EPA set new NAAQS provisions for particulate matter (PM) and ozone (commonly referred to as soot and smog). The standard for inhalable particles (PM_{10}) remains essentially unchanged, while a new standard for respirable particles ($PM_{2.5}$)—those measuring 2.5 micrometers in diameter and smaller—was established at an annual limit of 15 micrograms per cubic meter, with a 24-hour limit of 65 micrograms per cubic meter.



▲ Eight SCR catalysts with various shapes and compositions were evaluated side-by-side at Gulf Power's Plant Crist using high sulfur coal. NO_x reductions of 80 percent were achieved.

The proposed revisions to NAAQS for $PM_{2.5}$ also might require additional SO_2 control because many sulfur species are in this size range. Establishing reliable relationship between fine sulfate emissions and ambient $PM_{2.5}$ concentrations could have serious repercussions for coal burning facilities.

For ozone, the standard was tightened from 0.12 parts per million (or 120 parts per billion) of ozone measured over one-hour to a new standard of 0.08 parts per million (or 80 parts per billion) measured over eight-hours, with the average fourth highest concentration over a three-year period determining whether an area is out of compliance.

Air Toxics

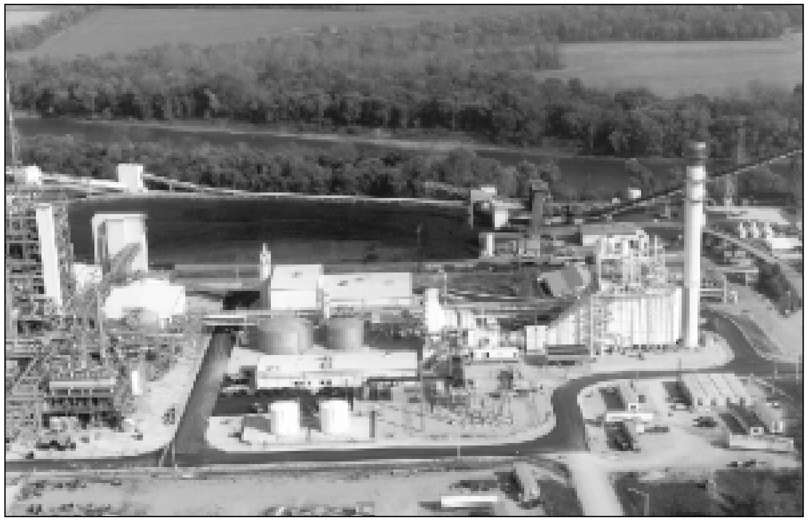
Under Title III of the CAAA, EPA is responsible for determining the hazards to public health posed by 189 hazardous air pollutants (HAPs) and is required to perform a study of HAPs to determine the public health risks that are likely to occur as a result of power plant emissions. The Department of Energy (DOE) recognizes the importance of detecting and measuring HAPs in stack gases and has implemented a program with industry to monitor HAPs emissions at CCT Program project sites. Two objectives of the HAPs monitoring are to (1) improve the quality of HAPs data being gathered and (2) monitor a broader range of plant configurations and emissions control equipment. As a result of this program, 21 CCT projects are monitoring HAPs, with 11 having been completed by September 1998 (see Appendix C Exhibit C-7).

In another effort begun in January 1993, EPA, with the participation of DOE under the Coal Research and Development Program, the Electric Power Research Institute (EPRI), and the Utility Air Regulatory Group (UARG), began an emissions data collection program using state-of-the-art sampling and analysis techniques. Emissions data were collected from eight utilities representing nine process configurations, several of which were sites for CCT projects. These utilities represented different coal types, process configurations, furnace types, and pollution control methods. The report, *A Comprehensive Assessment of Toxic Emissions from Coal-Fired Power Plants: Phase I Results from the U.S. Department of Energy Study*, was released in September 1996 and provided the raw data from the emissions testing. The second phase of the DOE/EPRI effort involves sampling at other sites, including the CCT Program's Wabash River, Tampa Electric, and Sierra Pacific integrated gasification combined-cycle (IGCC) projects.

In another DOE study, HAPs data were collected from 16 power plants and reported in *Summary of Air Toxics Emissions Testing at Sixteen Utility Plants*. The report, issued in July 1996, provides an assessment of HAPs measured in the coal, across the major pollution control devices, and emitted from the stack.

Following up on the October 1996 EPA report to Congress, *Study of Hazardous Air Pollutant Emissions from Electric Utility Steam Generating Units, Interim Final Report*, a new report has been released by EPA focusing on Mercury emissions. The December 1997 report, *Mercury Study Report to Congress*, estimates that the U.S. industrial sources were responsible for releasing 158 tons of Mercury into the atmosphere in 1994 and 1995. The EPA estimates that 87 percent of those emissions originate from combustion sources such as waste and fossil fuel facilities, 10 percent from manufacturing facilities, 2 percent from area sources, and 1 percent from other sources. The EPA also identified four specific categories that account for about 80 percent of the total anthropogenic sources: coal-fired power plants, 33 percent; municipal waste incinerators, 18 percent; commercial and industrial boilers, 18 percent; and medical waste incinerators, 10 percent. The next step for EPA is to assess the need for enhanced research on health effects and new pollution control technologies, community "right-to-know" approaches, and regulatory actions.

The results of the HAPs program have significantly mitigated concerns about HAPs emission from coal-fired power generation and focused attention on a few flue gas constituents. The results have the potential to make the forthcoming EPA regulations less strict, which could avoid unnecessary control costs and thus save consumers money on electricity bills.



▲ Hazardous air pollutants are being measured at the Wabash River IGCC unit.

Global Climate Change Protection

The CCT Program had its roots in the reduction of acid rain precursors and was responsive to the recommendations contained in the *Joint Report of the Special Envoys on Acid Rain* as discussed earlier. Twelve years later, the future of coal and clean coal technology may rest on the outcome of international concerns and negotiations on emissions of greenhouse gases (GHG), particularly carbon dioxide (CO_2).

In May 1992, the United States became a signatory to the U.N. Framework Convention on Climate Change (FCCC), which was ratified by Congress in October 1997. The FCCC directed Annex I parties (developed countries) to implement programs and actions aimed at returning GHG emissions to 1990 levels by 2000. As a result, the *Climate Change Action Plan*, published in October 1993, recommended a number of voluntary mitigation actions. In 1995, the first meeting of the Conference of Parties (COP-1) to the FCCC was held in Berlin, Germany. The purpose of this conference was to determine whether the non-binding FCCC was adequate. The conclusion was that most parties at COP-1 were not meeting the previously agreed to goals. As a result, the Berlin Mandate was adopted. The Berlin Mandate calls for negotiation of a protocol to enhance the commitments of Annex I parties for the period beyond 2000. The second meeting of the Conference of Parties (COP-2) held in Geneva, Switzerland, in July 1996, resulted in the Geneva Declaration calling for Annex I parties to adopt legally binding commitments by the Third Conference of Parties (COP-3) scheduled for Kyoto, Japan, in December 1997. At Kyoto, the following agreements were reached:

- A multi-year timeframe (2008-2012) for emission reductions;
- Five year averaging of emissions reductions;
- Differentiated targets for key industrial nations ranging from 6 to 8 percent below baseline levels (1990 and 1995), with the United States agreeing to a 7 percent reduction below a 1990 baseline;
- Allowance for certain activities, such as planting trees, that absorb carbon dioxide—called "sinks"—to be offset against emissions targets; and
- Inclusion of all six significant greenhouse gases (CO_2, methane, nitrous oxide, ozone, water vapor, and hydrofluorcarbons).

The agreement also includes flexible market mechanisms to allow countries to reach their targets, rather than "policies and measures," such as carbon taxes. Companies and countries will be able to trade emissions permits. However, the Kyoto agreement failed to meet U.S. demands for participation by developing countries.

The responsiveness and role of clean coal technologies in meeting GHG reduction goals of U.S. utilities is found in the *Climate Change Action Plan's* Climate Challenge Program. The basis of the program is described in the April 20, 1994, Memorandum of Understanding between DOE and representatives of the nation's electric utility industry—Edison Electric Institute, American Public Power Association; National Rural Electric Cooperative Association; Large Public Power Council; and the Tennessee Valley Authority.

The Climate Challenge Program consists of voluntary commitments by electric utilities to undertake actions to reduce, avoid, offset, or sequester GHG emissions. These commitments are formalized in individual utility Participation Accords for large utilities and in Letters of Participation for small utilities. The DOE provides technical information and support, reports on the progress of the program, and provides public recognition to utility participants. The types of commitments are broad enough so that any utility can participate, regardless of size, type, or amount of generation; resource mix; or load growth.

Clean coal technologies can play an important role in implementation of these Participation Accords. Improvements in generation technology, knowledge of how generation is operated and maintained, and optimal location of generation on the grid can have measurable beneficial effects on both GHG emissions and operating costs. Utilities are pursuing three broad strategies for reducing GHG emissions through more efficient power generation: (1) improving the efficiency of existing capacity, (2) repowering or replacing generation with more efficient generation, and (3) repowering or replacing generation with generation that uses lower-carbon fuels.

More than half of the Participation Accords include fossil-related activities. Fossil-related GHG reduction commitments total about 7.4 million metric tons of carbon equivalent in the year 2000, approximately one-sixth of all Climate Challenge Program tonnage commitments.

As part of its accord, CINergy has installed clean coal technology at the Wabash River Generating Station, which is owned by its subsidiary, PSI Energy. In a fully commercial setting, PSI Energy and its partner, Dynergy, are demonstrating coal gasification repowering of an existing unit. Where there was an aging, inefficient, little-used unit, there is now a very clean and highly efficient unit that will generate power into the next century. The original plant capacity was 100 MWe, but is now 262 MWe (net), and the original heat rate of 11,000 Btu per kilowatt-hour is now under 9,000, one of the lowest for commercial coal plants in the United States. Because the heat rate is so much lower, the rate of CO_2 emissions is decreased by about 20 percent relative to a conventional plant of the same size. Additionally, emissions of SO_2, NO_x, and particulate matter are reduced by at least 90 percent.

The 250-MWe Tampa Electric Company's integrated gasification combined-cycle project began operations in 1996. With a heat rate of 8,600 Btu per kilowatt-hour (40 percent efficiency), the plant's operation will result in a GHG emission reduction of over 20 percent when compared to conventional technology. Sierra Pacific Power Company's Piñon Pine integrated gasification combined-cycle (IGCC) project (99 MWe), which began operation in 1998, will result in similar reductions. Technologies such as pressurized fluidized-bed combustion and integrated gasification fuel cell, also being demonstrated under the CCT Program, represent other high-efficiency technology options for significant reduction of CO_2.

Finally, in an effort to increase the awareness of the role that clean coal technologies can have in meeting global climate concerns, the United States is participating in the International Energy Agency Greenhouse Gas Research and Development Program (IEA/GHG). The work conducted by the program focuses on technical and economic assessments and collaborative research on technology to address global concerns due to possible climate change resulting from atmospheric buildup of greenhouse gases. The IEA/GHG investigates and evaluates technical ways of reducing greenhouse gas emissions through improved fossil fuel technologies and by capture and sequestration of greenhouse gases. This program also serves as a source of independent expert data for policy makers, industry, and the public on coal technologies to address global climate concerns.

The IEA/GHG is conducting studies of a number of technologies, including many clean coal technologies. For example, completed studies address IGCC, advanced pulverized coal cycles, ocean sequestration of CO_2, and chemical utilization of CO_2. Examples of ongoing studies include integrated gasification fuel cells and IGCC using Orimulsion.

Value-Added Solid Waste

The CCT Program also addresses solid waste considerations. For example, two projects redefined the state-of-the-technology in wet flue gas desulfurization. Included in this significant technology improvement was production of commercial-grade gypsum in lieu of the scrubber sludge associated with conventional scrubbers of the early 1990s. Scrubber sludge had been projected to require over 4,500 acres per year for disposal by 2015. Advances under the CCT Program precluded that need. The balance of technologies in the CCT Program also address solid waste concerns by producing salable byproducts instead of wastes (e.g., sulfur, sulfuric acid, or fertilizer) or dry environmentally benign materials. These dry materials can either be used as construction materials (e.g., for use in soil and road bed stabilization, or as a cement ingredient), agricultural supplements, means to mitigate mine subsidence and acid mine drainage, or readily disposed of in landfills.

Coal Technologies for Competitive Performance

When the CCT Program started in 1986, the electric utility industry was highly regulated. The major uncertainty was the breadth and depth of environmental regulatory requirements that would be imposed on the industry. Even this uncertainty was mitigated by the fact that the environmental control costs could be passed through to the consumer if approved by the state regulatory commission. As long as the utility made prudent investments in plant and equipment, their economic future was fairly stable and predictable. Most industry observers assumed that coal and nuclear energy would carry the burden of baseload generation, oil would be phased out, and natural gas would be used for meeting peak load requirements.

By mid-1997, the picture was entirely different—the utility industry was in the midst of a major restructuring to accommodate a competitive marketplace. This restructuring was driven by legislative, consumer, and technology factors as follows:

- Consumers became a major factor in pushing for competition and regulatory reform even though regulators provide the oversight necessary to assure consumers were paying a fair price. However, the price differential among the states and regions of the country meant that large industrial users of electricity in some areas were burdened with high electricity prices, while their competitors in other areas had access to much lower cost electricity and thus a competitive production cost edge.

- The Public Utility Regulatory Policies Act of 1978 (PURPA) and the Energy Policy Act of 1992 (EPAct) were two major legislative factors. Under PURPA, utilities were required to purchase electricity from certain "qualified facilities" (QFs) at a price equal to the utility's estimated avoided cost. As a result, the amount of electricity generated by these nonutility power producers increased dramatically to over 280 billion kilowatt-hours or about 10 percent of the utility generation in 1995. The EPAct, in amending the Public Utility Holding Company Act of 1935 (PUHCA) and the Federal Power Act of 1935 (FPA) lifted more of the constraints on the development of nonutility generation as well as some of the restrictions on competition in wholesale electricity markets.

- The EPAct created a new class of producer called the exempt wholesale generator (EWG), which is defined as "any person determined by the Federal Energy Regulatory Commission to be engaged directly through one or more affiliates—and exclusively in the business of owning or operating—all or part of one or more eligible facilities and selling electric energy at wholesale." This amendment to PUHCA provided that nonutility companies could develop EWGs without coming under the provisions of PUHCA and exempt holding companies could also develop EWGs without losing their exemption from PUHCA. Any EWG also in the retail utility's rate base had to receive state regulatory approval before it could be exempted from PUHCA. The EPAct specifically allowed both registered and exempt holding companies to own, acquire, and operate EWGs. The law also allowed for so-called "hybrid plants," which have ownership divided between utility companies, whose portion is included in the rate base, and EWGs, whose portion is exempt. The act sought to limit the abuse of affiliate transactions by prohibiting an electric utility company from purchasing wholesale energy from an EWG that was one of its affiliates. Unlike PURPA, the PUHCA reforms did not guarantee EWGs a market for their power, thereby requiring that the EWGs compete with power from other sources in the wholesale power market.

- The EPAct further promoted wholesale competition by mandating that transmission facility owners must provide open access to the grid by wheeling power to wholesale customers at cost-based rates. Furthermore, anyone may petition the FERC for access to the transmission grid. On April 14, 1996, the FERC issued two closely related orders, Order Nos. 888 and 889, detailing rules to assure nondiscriminatory open access to interstate electricity transmission and recovery of the utilities' prudently incurred costs. Order Nos. 888-A, 888-B, 889-A, and 889-B were subsequently issued clarifying and modifying positions in the original orders. The orders are currently being appealed.

- Consumer pressures for access to lower priced power have been successful in bringing about competition in retail as well as wholesale power markets. Deregulation of retail markets is occurring at the state level. (FERC is prohibited from ordering retail wheeling.) Under the EPAct, states continue to have responsibility for regulating (1) any electric company operating within its jurisdiction, (2) any EWG selling electricity wholesale to such a utility, and (3) any holding company that was an associate or affiliate of an EWG selling power to a regulated utility. By the end of Fiscal Year 1998, twelve states have enacted legislation to allow competition in the retail electricity market in one form or another. In six other states, there have been comprehensive regulatory orders issued. Legislation or regulatory action is pending in another six states. Twenty-four states and the District of Columbia are currently investigating deregulation options. Only in two states is there no significant deregulation activity. Under retail deregulation, end users are not required to purchase power from their local utility company, but instead may purchase power from generators or marketers located in other states and regions of the country. In this competitive market environment, power is priced according to market conditions, not necessarily according to generation costs.

- Advances in the technology of electricity production are another factor that has had an impact on restructuring. Nonutility generators have taken advantage of these advances, such as aero-derived gas turbines, to generate electricity cheaper than can be achieved using conventional fossil steam or nuclear generators. The new technologies are often more efficient, less environmentally obtrusive, and can be installed in a very short period of time in capacity modules closely matching the load growth curves.

- Also, federal legislation on utility restructuring seems imminent as a number of bills are being debated.

These factors have had a pronounced effect on the utility market for coal and clean coal technology. A comparison of 1985 and 1997 energy projections for coal, natural gas, and oil, shown in Exhibit 1-3, illustrates the magnitude of the change that restructuring is playing, as well as environmental regulation discussed previously. Coal is projected to maintain its lead in the production of electricity in 2010 at 49 percent; however, that is down from 60 percent when the CCT Program started. The differential has been, for the most part, made up by the growth in natural gas power generation. Nuclear power's contribution to the nation's electric power generation in 2010 has dropped by 28 percent between the 1985 and 1997 projections.

Industry restructuring and competition will impact coal and coal technologies for the foreseeable future. Utilities are expected to improve their operating efficiencies by using existing plants at higher capacity factors. Contributing to increased capacity factors is a projected drop in generating capacity not only from nuclear plant retirements but capacity losses where stranded costs are not recovered. The EIA has projected that the capacity factor for coal-fired power plants will increase from 66 percent in 1996 to 80 percent in 2020. The EIA projects natural gas-fired generation to grow from over 462 billion kilowatt-hours in 1996 to 1,583 billion in 2020, most of that using combined-cycle technology. EIA further predicts that no net coal-fired capacity additions will be made until 2010, when rising natural gas costs and nuclear and coal retirements are projected to cause increasing demand for capacity. At that time, new highly efficient low-emissions power systems will enter the power production markets. New concepts to reduce delivered electricity prices will likely be employed. Examples include minemouth plants that reduce or eliminate the coal transportation cost component in power production. Also, cogeneration and coproduction systems will be available, which allow the consumer's cost of electricity to be offset by the profitability of coproducts.

The CCT Program is demonstrating the first commercial versions of the advanced high-efficiency coal systems that will be needed when older plants are retired and new capacity additions are needed to assure continued low-cost reliable electric power service. The CCT Program is also demonstrating technologies to produce clean fuels. Processes to remove precursors to acid rain and HAPs represent a pollution prevention approach that is an integral part of efforts to develop advanced coal-based power for the future.

Exhibit 1-3
Comparison of Energy Projections

	Electricity Sales (10^9 kWh)			Coal Consumption (10^6 tons)			Gas Consumption[a] (10^{12} ft^3)			Oil Consumption[a] (10^6 barrels)		
	A	B	% dif	A	B	% dif	A	B	% dif	A	B	% dif
1995	3,018	3,026	0.3	924	958	3.7	3.0	3.37	12	0.2	0.30	50
2000	3,384	3,318	-2.0	1,059	1,058	-0.1	2.7	4.05	50	0.6	0.24	-60
2010	4,176	3,877	-7.2	1,355	1,162	-14.2	1.7	7.22	325	0.4	0.16	-60

A *National Energy Policy Plan Projections to 2010,* U.S. Department of Energy, December 1985.
B *Annual Energy Outlook 1998 with Projections to 2020,* Energy Information Agency, December 1997.

% dif = percent difference between the two projections.

[a] Consumptions by electric generators excluding cogenerators.

Coal Technologies to Sustain Economic Growth

It is in the national interest to maintain a multi-fuel energy mix to sustain national economic growth. Coal is a key component of national energy security because of its affordability, availability, and abundancy within the nation's borders. The CCT Program's strategy leads to the development and deployment of a technology portfolio that enhances the efficient use of this coal resource while assuring national and global environmental goals are achieved. The domestic coal resources are large enough to supply U.S. needs for more than 250 years at current rates of production.

The United States is increasingly dependent on imported oil as low prices have resulted in decreased domestic oil production for 13 years. That trend was broken in 1995 by an oil production capacity increase of 0.4 million barrels per day. In 1996, net petroleum imports were 8.5 million barrels per day, or 46 percent of domestic consumption. In its latest projections for 2020, EIA expects imports to range from 13.8 to 18.4 million barrels per day depending on oil price. The EIA reference case for 2020 calls for net imports of 16.0 million barrels per day, which is equivalent to over 66 percent of consumption. Also, natural gas imports are expected to grow from 12.4 percent of total gas consumption in 1996 to 15.3 percent in 2020. These imports are primarily from Canada, which does not represent a supply stability problem, but does represent a drain on balance of payments.

United States coal consumption is equivalent to approximately 10 million barrels of oil per day and represents a reduction in balance of payments of over $50 billion per year. The CCT Program will provide the technologies that will enable coal to continue as a major component in the nation's economy while achieving the environmental quality that society demands. The domestic and export value of 1996 coal production approaches $23.2 billion in the U.S. economy. Coal related jobs are dispersed through the mining, transportation, manufacturing, utility, and supporting industries.

A U.S. coal conversion industry could directly reduce the nation's dependency on imported oil. The economic impact of adding to domestic oil production or reducing the cost of imported oil is very significant. The CCT Program is responding to this opportunity through development and demonstration of mild gasification and liquid-phase methanol production technologies.

In 1996, the U.S. exported 90 million tons of coal to more than 40 nations. Coal exports to foreign destinations contributed $3.39 billion to the U.S. balance of payments in 1997. Worldwide demand for energy is expected to reach 639 quadrillion Btu by 2020, over 1.7 times the current level. According to the EIA, worldwide coal use in 1995 accounted for about 25 percent of total energy consumption and 36 percent of the energy consumed worldwide for electricity generation. Those market shares are not projected to change substantially through 2020. Exports of U.S. coal are projected to increase to over 128 million tons by 2020.

The worldwide market for power generation technologies could be as high as $2.3 trillion between 1995 and 2010. Roughly two-thirds of the investment will be in developing countries. This market provides opportunities for U.S. technology suppliers, developers, architect/engineers, and other U.S. firms to capitalize on the advantages gained through experiences in the CCT Program. However, aggressive action is needed as other governments are recognizing the enormous economic benefits that their economies can enjoy if their manufacturers capture a greater share of this market.

Beyond the CCT Program, DOE activities are aimed at creating a favorable export climate for U.S. coal and coal technology. These efforts will: (1) improve the visibility of U.S. firms and their products by establishing an information clearinghouse and closer liaison with U.S. representatives in other countries, (2) strengthen interagency coordination of federal programs pertinent to these exports, and (3) improve current programs and policies for facilitating the financing of coal-related projects abroad.

▲ National energy security is enhanced by coal liquefaction technology being demonstrated at the Eastman Chemical Company in Kingsport, TN. Air Products and Chemical's liquid phase methanol process is producing 80,000 gallons per day of methanol from eastern high-sulfur bituminous coal.

Coal Technology for the Future

DOE has structured an integrated Coal and Power Systems Research, Development, and Demonstration (RD&D) Program with the mission to foster the development and deployment of advanced, clean, affordable power systems and technologies for the clean utilization of coal. The R&D Program is designed to assure an ample, secure, clean, low-cost domestic electricity and domestic fuel supply through viable technical options. Contributions of the RD&D Program toward achieving national energy policy goals include:

- Improving the efficiency of the energy system,
- Ensuring against energy disruptions,
- Promoting energy production and use in ways that respect health and environments,
- Expanding future energy choices, and
- Cooperating internationally on energy issues.

Vision 21

Vision 21 PowerPlex. DOE's Fossil Energy RD&D program builds on the CCT Program toward realizing a "Vision 21 PowerPlex"—a modular facility capable of using a multiplicity of fuels (such as coal, biomass, gas, petroleum coke, and municipal waste) to competitively produce a number of commodities (such as electricity, steam, fuels, and chemicals) at efficiencies greater than 60 percent and with near zero pollutant emissions.

A Vision 21 PowerPlex represents a suite of technology modules that can be interconnected in different configurations to produce selected products. When coupled with CO_2 capture and recycling or sequestration, Vision 21 systems would create no environmental impact outside of their physical "footprint."

Exhibit 1-4 graphically illustrates the Vision 21 concept. Core technology and enabling technology thrusts are outlined below.

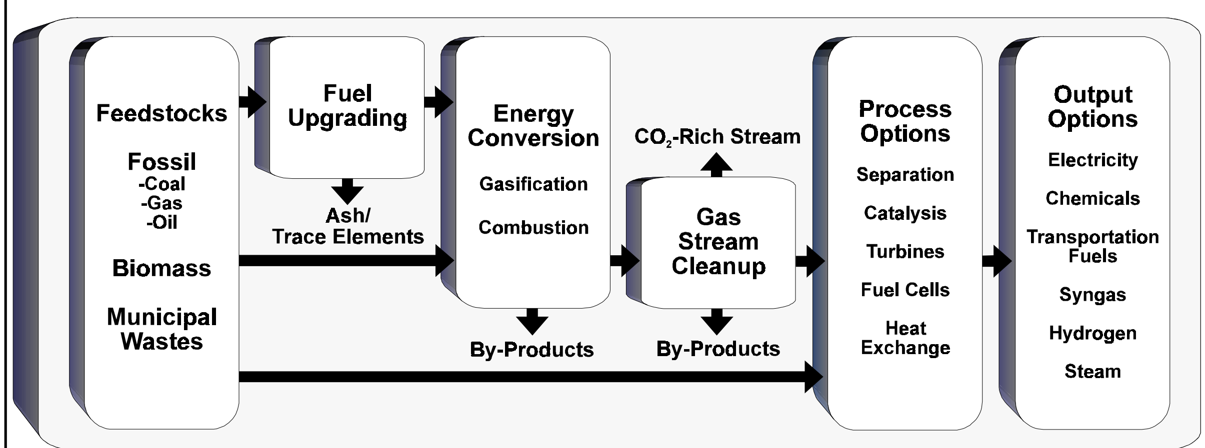
Vision 21 Core Technologies

Fuel-Flexible Gasification. Gasification is a key core technology because the syngas produced from carbon-based feedstocks can be used as fuel for a gas turbine in an integrated gasification combined-cycle electric power generation mode, a source of hydrogen for a fuel cell, feedstock for production of chemicals, or a fuel gas for industrial applications. RD&D will address how best to gasify fuel mixtures such as coal and biomass.

High-Performance Combustion. Combustion remains a primary energy conversion process that can be used in conjunction with other approaches such as gasification. The RD&D challenge will be to significantly improve on efficiency and pollutant control through combustion modification and integration of other process technologies such as gasification and high temperature heat exchangers, particulate filtration, and advanced gas turbines.

Fuel Cell/Turbine Hybrids. Fuel cells and gas turbines represent important energy supply technologies historically on two separate development paths. Under Vision 21, concepts will be pursued to integrate the two technologies and adapt them to operate on a multiplicity of fuels.

Exhibit 1-4
Vision 21 PowerPlex



Gas Separation Technologies. Advanced membrane technology shows promise for separating two key elements used in energy supply technologies—oxygen and hydrogen—from air and process streams. Membrane RD&D will be pursued because it has the potential to significantly reduce the cost of the existing energy intensive methods—cryogenic air separation is currently used to produce oxygen for gasification and natural gas reforming is used to produce hydrogen for fuel cells.

Vision 21 Enabling Technologies

Materials. The drive to higher efficiency requires operation at ever increasing temperatures and pressures in corrosive environments. To realize efficiency goals, materials will be developed with the requisite strength and resistance to corrosion and high-temperature.

Catalysts and Sorbents. Improved catalysts offer the means to reduce the energy needed to affect conversion in such areas as coal to liquid fuels or chemicals. Sorbents that can operate effectively at high temperatures mitigate heat losses associated with lowering process temperatures to accommodate conventional sorbents. Progress in catalyst and sorbent performance will be pursued because of the direct efficiency gains possible.

Instrumentation. The flexibility desired in Vision 21 plants to adjust to changing feedstocks and production requirements necessitates new control systems. RD&D will link artificial intelligence with sensors for key parameters to measure, process, and resolve the myriad of inputs necessary to affect optimum performance.

"Virtual" Plants. Scarce resources dictate less reliance on hardware testing and more reliance on predictive models in developing new technologies. Vision 21 efforts will increasingly rely on new computer simulation technologies to test processes and verify engineering performance, requiring development of advanced computation techniques similar to those used today to design commercial airplanes or to simulate nuclear explosions.

Carbon Sequestration. The means to capture and either recycle or permanently store CO_2 will also be sought. In conjunction with Vision 21, carbon sequestration would close the carbon cycle for fossil energy-based systems and eliminate the threat of global climate change.

▲ ➤ RD&D assures that clean, affordable coal technologies will be available in the future. Air Product's LaPorte coal liquefaction test facility (above) and Southern Company Services' Wilsonville power system development facility (right) contribute to RD&D efforts.

2. Program Implementation

Introduction

The CCT Program founding principles and implementing process resulted in one of the most successful cost-shared government/industry partnerships forged to date to respond to critical national needs. Through five nationwide competitions, a total of 60 government/industry cost-shared projects were selected, of which 40 valued at more than $5.6 billion have either been completed or remain active at the end of Fiscal Year 1998. For the 40 projects, the industry cost-share is an unprecedented 66 percent. Over 57 percent of the projects (23) have reached successfully completed operations. The balance are moving forward, with operational testing under way for eight projects

Over the nine-year period of soliciting and awarding projects, the thrust of the environmental concerns relative to coal use changed. Nevertheless, the adopted implementing process allowed the program to remain responsive to the changing needs. The result is a portfolio of technologies and a data base that will enable coal to remain a major contributor to the U.S. energy mix without being a threat to the environment. This result will ensure secure, low-cost energy requisite to a healthy economy well into the 21st century.

Success of the CCT Program is measured by the degree to which the operational, environmental, and economic performance of a technology can be projected for commercial applications. Decision-makers must have a sufficient database to project performance and assess associated risk for commercial introduction and deployment of new technologies. This measure was a driving force in establishing the principles that created the foundation for the implementation process. The government role is non-traditional, moving away from a command-and-control approach to a performance-based approach, where the government sets performance objectives and industry responds with its ideas and is allowed broad latitude in technical management of the projects. This approach encourages technology innovation and cost-sharing. Industry and the public play major roles in the process, reflecting their respective roles in moving technologies into the marketplace.

Implementation Principles

The principles underlying the CCT Program were developed after much study of previous government demonstration programs, those meeting with both positive and negative results. Together, the principles represent a composite of incentives and checks and balances that allows all participants to best apply their expertise and resources. These guiding principles are outlined below.

- **A strong and stable financial commitment exists for the life of the projects.** Full funding for the government's share of selected projects was appropriated by Congress at the outset of the program. This up-front commitment has been vital to getting industry's response in terms of quantity and quality of proposals received and the achievement of 66 percent cost-sharing.
- **Multiple solicitations spread over a number of years enabled the program to address a broad range of national needs with a portfolio of evolving technologies.** Allowing time between solicitations enabled Congress to adjust the goals of the program to meet changing national needs, provided DOE time to revise the implementation process based on lessons learned in prior solicitations, and provided industry the opportunity to develop better projects and more confidently propose evolving technologies.
- **Demonstrations are conducted at commercial scale in actual user environments.** Typically, a technology is constructed at commercial scale with full system integration, reflective of its intended commercial configuration, and operated as a commercial facility or installed on an existing commercial facility. This enables the technology's performance potential to be judged in the intended commercial environment.
- **The technical agenda is determined by industry, not the government.** Based on goals established by Congress and policy guidance received, DOE set definitive performance objectives and performance-based evaluation criteria against which proposals would be judged. Industry was given the flexibility to use their expertise and innovation to define the technology and proposed project in response to the objectives and criteria. DOE

selected the projects based on those that best met the evaluation criteria.

- **Roles of the government and industry are clearly defined and reflect the degree of cost-sharing required.** The government plays a significant role up front in structuring the cooperative agreements to protect public interests. This includes negotiating definitive performance milestones and decision points throughout the project. Once the project begins, the industrial participant is responsible for technical management, while the government oversees the project through aggressive monitoring and engages in implementation only at decision points. Continued government support is assured as long as project milestones and the terms and conditions of the original cooperative agreement continue to be met.

- **At least 50 percent cost-sharing is required throughout all project phases.** Industry's cost-share was required to be tangible and directly related to the project, with no credit for previous work. By sharing essentially in each dollar expended along the way, on at least an equal basis, industry's commitment to fulfilling project objectives was strengthened.

- **Allowance for cost growth provides an important check-and-balance feature to the program.** Statutory provisions allow for additional financial assistance beyond the original agreement in an amount up to 25 percent of DOE's original contribution. Such financial assistance, if provided, must be cost-shared by the industrial participant at no less than the cost-share ratio of the original cooperative agreement. This statutory provision recognizes the risk involved in first-of-a-kind demonstrations by allowing for cost growth. At the same time, it recognizes the need for the industrial participant's commitment to share cost growth and limits the government's exposure.

- **Industry retains real and intellectual property rights.** The level of cost-sharing warrants the industrial participant retaining intellectual and real property rights and removes potential constraints to commercialization. Industry would otherwise be reluctant to come forward with technologies they have developed to the point of demonstration, relinquishing their competitive position.

- **Industry must make a commitment to commercialize the technology.** Consistent with program goals, the industrial participant is required to make the technology available on a nondiscriminatory basis to all U.S. companies that seek, under reasonable terms and conditions, to use the technology. While the technology owner is not forced to divulge know-how to a competitor, the technology must be made available to potential domestic users on reasonable commercial terms.

- **Upon successful commercialization of the technology, repayment up to the government's cost-share is required.** The repayment obligation occurs only upon successful commercialization of the technology. It is limited to the government's level of cost-sharing and the 20-year period following the demonstration.

In summary, there are built-in checks and balances to ensure that the industry and government roles are appropriate and that the government serves as a risk-sharing partner without impeding industry from using its expertise and getting the technology into the marketplace.

Implementation Process

Significant public and private sector involvement was integral to the process leading to technology demonstration and critical to program success. Even before engaging in a solicitation, a public process was instituted under the National Environmental Policy Act (NEPA) to review the environmental impacts. A programmatic environmental impact assessment (PEIA), followed by a programmatic environmental impact statement (PEIS), was prepared prior to initiating solicitations. Public comment and resolution of comments were required prior to proceeding with the program.

As to the solicitation process, Congress set the goals for each solicitation in the enabling legislation and report language (see Appendix A for legislative history and Appendix B for program implementation history). The Department of Energy translated the congressional guidance and direction into performance-based criteria and developed approaches to address lessons learned from previous solicitations. Before proceeding with a solicitation, however, an outline of the impending solicitation and attendant issues and options was presented in a series of regional public meetings to obtain feedback. The public meetings were structured along the lines of workshops to facilitate discussion and obtain comments from the broadest range of interests. Comments from the public meetings were then used in preparing a draft solicitation, which in turn was issued for public comment. Comments received were formally resolved prior to solicitation issuance.

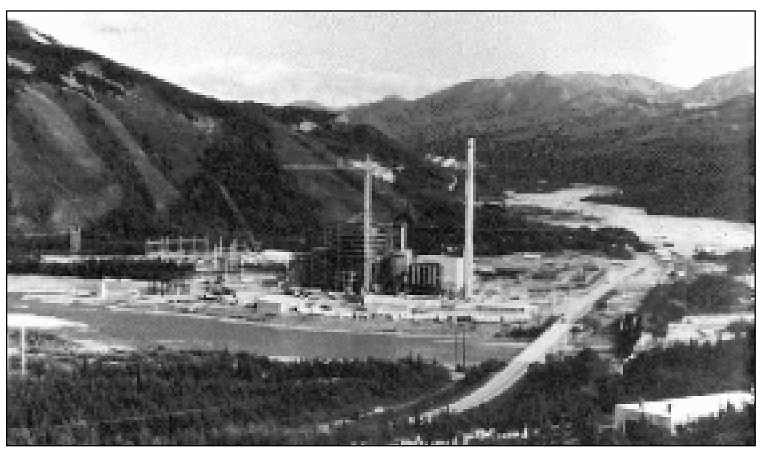
To aid proposers, preproposal conferences were held for the purpose of clarifying any aspects of the solicitation. Further, every attempt was made in the solicitation to impart a clear understanding of what was being sought, how it would be evaluated, and what contractual terms and conditions would apply. A section of the solicitation was devoted to helping potential proposers determine technology eligibility, and numerical quantification of the evaluation criteria was provided. The solicitation also contained a model cooperative agreement with the key relevant contractual terms and conditions.

Project selection and negotiation leading to award were conducted under stringent rules carrying criminal penalties for non-compliance. Proposals were evaluated and projects negotiated strictly against and within the criteria and terms and conditions established in the solicitation. In the spirit of NEPA, information required and evaluated included project-specific environmental, health, safety, and socioeconomic aspects of project implementation.

Upon project award, another public process was engaged to ensure that all site-specific environmental concerns were addressed. The National Environmental Policy Act requires that a rigorous environmental assessment be conducted to address all potential environmental, health, safety, and socioeconomic impacts associated with the project. The findings can precipitate a more formal environmental impact statement (EIS) process, or the findings can remain as an environmental assessment (EA) along with a finding of no significant impact (FONSI). During the EIS process, public meetings are held for the purpose of disclosing the intended project activities, with emphasis on potential environmental, health, safety, socioeconomic impacts, and planned mitigating measures. Comments are sought and must be resolved before the project can proceed. This process has led to additional actions taken by the industrial participant beyond the original project scope. To facilitate the NEPA process, DOE encouraged environmental data collection through cost-sharing during the negotiation period contingent upon project award.

Because of the environmental nature of the CCT Program, DOE took a proactive posture in carrying out the principles of NEPA. Environmental concerns were aggressively addressed and the public engaged prior to major expenditure of public funds. Furthermore, DOE required that an in-depth environmental monitoring plan (EMP) be prepared, fully assessing potential pollutant emissions, both regulated and unregulated, and defining the data to be collected and the methodology for collection. All cooperative agreements required preparation of environmental monitoring reports that provide results of the monitoring activities. As environmental issues emerged, every effort was made to address them directly with the understanding that commercial technology acceptance hinged on satisfying users and the public as to acceptable environmental performance. Appendix C reviews the proactive environmental stance taken by the program, further delineates the NEPA process, and provides the status of key actions.

▼ The NEPA process assured environmental acceptability of the Healy Clean Coal Project on the border of Denali National Park in Alaska.



Projects are managed by the participant, not the government. However, public interests are protected by requiring defined periods of performance referred to as budget periods, throughout the project. Budget periods are keyed to major decision points. A set amount of funds are allotted to each budget period, along with performance criteria to be met before receiving funds for the next budget period. These criteria are contained in project evaluation plans (PEPs). Progress reports and meetings during budget periods serve to keep the government informed. At the decision points, progress against PEPs is formally evaluated, as is the PEP for the next budget period. Financial data is also examined to ensure the participant's capability to continue required cost-sharing. Failure to perform as expected results in greater government involvement in the decision-making process. Proposal of major project changes precipitates not only in-depth programmatic assessment, but legal and procurement review as well. Decisions regarding continuance into succeeding budget periods, any increase in funding, or major project changes require the approval of the Assistant Secretary with program responsibility.

Beyond the formal process associated with the solicitations, parallel efforts were conducted to inform stakeholders of ongoing events, results, and issues, and to engage them in discussion on matters pertinent to ensuring that the program remained responsive to needs. A continuing dialog was facilitated by direct involvement in the projects of a large number of utilities, technology suppliers, and states, as well as key industry-based research organizations (e.g., the Electric Power Research Institute and Gas Research Institute). This was accompanied by executive seminars designed to enhance communications with the utility, independent power production, regulatory, and financial sectors. The approach was to identify those sectors where inputs were missing and then structure seminars to provide information on the program and obtain the executives' perspectives and suggestions for enhancing program performance. Furthermore, an annual CCT Conference was instituted to serve as a forum for updating progress and results and discussing issues effecting the outcome of the CCT Program. And, an outreach program was put in place to ensure that needed information was prepared and disseminated in the most efficient manner, leveraging a variety of domestic and international conferences, symposia, and workshops. These activities are discussed in further detail in Section 4.

During implementation of the CCT Program, many precedent-setting actions were taken and many innovations were used by both the public and private sectors to overcome procedural problems, create new management systems and controls, and move toward accomplishment of shared objectives. The experience developed in dealing with complex business arrangements of multi-million-dollar CCT projects is a significant asset that has contributed greatly to the CCT Program's success—an asset of value to other programs seeking to forge government/industry partnerships. To document lesson learned, *Clean Coal Technology Program Lessons Learned* was published in July 1994. This report documents the knowledge acquired over the course of the CCT Program through the completion of five solicitations. The report was based on the belief that it is of mutual advantage to the private and public sectors to identify those factors thought to contribute to the program's success and to point out pitfalls encountered and corrective actions taken.

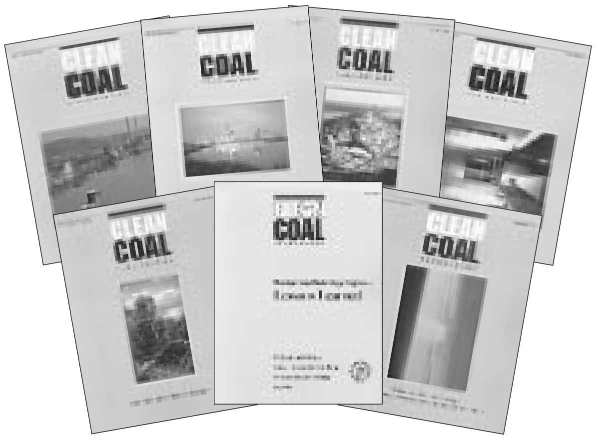
Commitment to Commercial Realization

The CCT Program has been committed to commercial realization since its inception. The significant environmental, operational, and economic benefits of the technologies being demonstrated in the program will be realized when the technologies achieve widespread commercial success. The importance attached to commercial realization of clean coal technologies is highlighted in Senate Report 99-82, which contains the following recommendation for project evaluation criteria: "The project must demonstrate commercial feasibility of the technology or process and be of commercial scale of such size as to permit rapid commercial scale-up."

The commitment to commercial realization recognizes the complementary but distinctive roles of the technology owner and the government. It is the technology owner's role to retain and use the information and experience gained during the demonstration and to promote the utilization of the technology in the domestic and international marketplace. The detailed operational, economic, and environmental data and the experience gained during the demonstration are vital to efforts to commercialize the technology. The government's role is to capture, assess, and transfer operational, economic, and environmental information to a broad spectrum of the private sector and international community. The information must be sufficient to allow potential commercial users to confidently screen the technologies and to identify those meeting operational requirements. The importance of commercial realization is confirmed by the requirement in the solicitations and cooperative agreements that the project participant must pursue commercialization of the technology after successful demonstration.

Each of the five solicitations contained requirements for the project proposals to include a discussion of the commercialization plans and approaches to be used by the participants. The proposer was required to discuss the following topics:

- The critical factors required to achieve commercial deployment, such as financing, licensing, engineering, manufacturing, and marketing;
- A timetable identifying major commercialization goals and schedule for completion;
- Additional requirements for demonstration of the technology at other operational scales, as well as significant planned parallel efforts to the demonstration project, that may affect the commercialization approach or schedule; and
- The priority placed by senior management on accomplishing the commercialization effort and how the project fits into the various corporation's business, marketing, or energy utilization strategies.



▲ Publications keep stakeholders informed of CCT Program contributions.

The cooperative agreement contains three mechanisms to ensure that the demonstrated technology can be replicated by responsible firms while protecting the proprietary commercial position of the technology owner. These three mechanisms are:

- The commercialization clause requires the technology owner to meet U.S. market demands for the technology on a nondiscriminatory basis (this clause "flows down" from the project participant to the project team members and contractors);
- The clauses concerning rights to technical data deal with the treatment of data developed jointly in the project as well as data brought into the project; and
- The patent clause affords protection for new inventions developed in the project.

In addition to ensuring the implementation of the above project-specific mechanisms, the government role also includes disseminating the operational, environmental, and economic performance information on the technologies to potential customers and stakeholders. To carry out this role, a CCT Outreach Program was established to perform the following functions:

- Make the public and local, state, and federal government policy makers aware of the CCTs and their operational, economic and environmental benefits;
- Provide potential domestic and foreign users of the technologies with the information needed for decision making;
- Inform financial institutions and insurance underwriters about the advancements in technology and associated risk mitigation to increase confidence; and
- Provide customers and stakeholders opportunities for feedback on program direction and information requirements.

Specific accomplishments of the CCT Outreach Program are discussed in Section 4 under Market Communications–Outreach.

Solicitation Results

Each solicitation was issued as a Program Opportunity Notice (PON)—a solicitation mechanism for cooperative agreements where the program goals and objectives are defined but the technology is not. Proposals for demonstration projects consistent with the objectives of the PON were submitted to DOE by specific deadlines. DOE evaluated, selected, and negotiated projects strictly within the bounds of the PON provisions. Award was made only after Congress was allowed 30 in-session days to consider the projects as outlined in a *Comprehensive Report to Congress* issued after each solicitation.

Exhibit 2-1 summarizes the results of solicitations. Exhibit 2-2 identifies the projects currently in the CCT Program and the solicitation under which the projects were selected. Appendix B provides a summary of the procurement history and a chronology of project selection, negotiation, restructuring, and completion or termination. Project sites are mapped in Exhibits 2-3 through 2-6, which indicate the geographic locations of projects by application category.

The resultant projects have achieved broad-based industry involvement. More than 55 individual electric generators serving 33 states have participated in the program. These utilities generate more than 178,000

Exhibit 2-1
CCT Program Selection Process Summary

Solicitation	PON Issued	Proposals Submitted	Projects Selected	Projects in CCT Program as of Sept. 30, 1998
CCT-I	February 17, 1986	51	17	8
CCT-II	February 22, 1988	55	16	9
CCT-III	May 1, 1989	48	13	13
CCT-IV	January 17, 1991	33	9	6
CCT-V	July 6, 1992	24	5	4
		211	60	40

Exhibit 2-2
Clean Coal Technology Demonstration Projects by Solicitation

Project and Participant	Location
CCT-I	
Development of the Coal Quality Expert™ (ABB Combustion Engineering, Inc., and CQ Inc.)	Homer City, PA
LIMB Demonstration Project Extension and Coolside Demonstration (The Babcock & Wilcox Company)	Lorain, OH
Advanced Cyclone Combustor with Internal Sulfur, Nitrogen, and Ash Control (Coal Tech Corporation)	Williamsport, PA
Enhancing the Use of Coals by Gas Reburning and Sorbent Injection (Energy and Environmental Research Corporation)	Hennepin and Springfield, IL
Tidd PFBC Demonstration Project (The Ohio Power Company)	Brilliant, OH
Advanced Coal Conversion Process Demonstration (Rosebud SynCoal Partnership)	Colstrip, MT
Nucla CFB Demonstration Project (Tri-State Generation and Transmission Association, Inc.)	Nucla, CO
JEA Large Scale CFB Combustion Demonstration Project	Jacksonville, FL
CCT-II	
SNOX™ Flue Gas Cleaning Demonstration Project (ABB Environmental Systems)	Niles, OH
Demonstration of Coal Reburning for Cyclone Boiler NO_x Control (The Babcock & Wilcox Company)	Cassville, WI
SO_x-NO_x-Rox Box™ Flue Gas Cleanup Demonstration Project (The Babcock & Wilcox Company)	Dilles Bottom, OH
Cement Kiln Flue Gas Recovery Scrubber (Passamaquoddy Tribe)	Thomaston, ME
Advanced Flue Gas Desulfurization Demonstration Project (Pure Air on the Lake, L.P.)	Chesterton, IN
Demonstration of Advanced Combustion Techniques for a Wall-Fired Boiler (Southern Company Services, Inc.)	Coosa, GA
Demonstration of Innovative Applications of Technology for the CT-121 FGD Process (Southern Company Services, Inc.)	Newnan, GA
Demonstration of Selective Catalytic Reduction Technology for the Control of NO_x Emissions from High-Sulfur-Coal-Fired Boilers (Southern Company Services, Inc.)	Pensacola, FL
180-MWe Demonstration of Advanced Tangentially Fired Combustion Techniques for the Reduction of NO_x Emissions from Coal-Fired Boilers (Southern Company Services, Inc.)	Lynn Haven, FL
CCT-III	
Commercial-Scale Demonstration of the Liquid-Phase Methanol (LPMEOH™) Process (Air Products Liquid Phase Conversion Company, L.P.)	Kingsport, TN
10-MWe Demonstration of Gas Suspension Absorption (AirPol, Inc.)	West Paducah, KY
Healy Clean Coal Project (Alaska Industrial Development and Export Authority)	Healy, AK
Full-Scale Demonstration of Low-NO_x Cell Burner Retrofit (The Babcock & Wilcox Company)	Aberdeen, OH

Exhibit 2-2 (continued)
Clean Coal Technology Demonstration Projects by Solicitation

Project and Participant	Location
CCT-III (continued)	
Confined Zone Dispersion Flue Gas Desulfurization Demonstration (Bechtel Corporation)	Seward, PA
Blast Furnace Granular-Coal Injection System Demonstration Project (Bethlehem Steel Corporation)	Burns Harbor, IN
McIntosh Unit 4A PCFB Demonstration Project (City of Lakeland, Lakeland Electric)	Lakeland, FL
ENCOAL® Mild Coal Gasification Project (ENCOAL Corporation)	Gillette, WY
Evaluation of Gas Reburning and Low-NO_x Burners on a Wall-Fired Boiler (Energy and Environmental Research Corporation)	Denver, CO
LIFAC Sorbent Injection Desulfurization Demonstration Project (LIFAC–North America)	Richmond, IN
Integrated Dry NO_x/SO_2 Emissions Control System (Public Service Company of Colorado)	Denver, CO
Tampa Electric Integrated Gasification Combined-Cycle Project (Tampa Electric Company)	Mulberry, FL
Commercial Demonstration of the NOXSO SO_2/NO_x Removal Flue Gas Cleanup System (NOXSO Corporation)	To be determined
CCT-IV	
Micronized Coal Reburning Demonstration for NO_x Control (New York State Electric & Gas Corporation)	Lansing and Rochester, NY
Milliken Clean Coal Technology Demonstration Project (New York State Electric & Gas Corporation)	Lansing, NY
Piñon Pine IGCC Power Project (Sierra Pacific Power Company)	Reno, NV
Pulse Combustor Design Qualification Test (ThermoChem, Inc.)	Baltimore, MD
Wabash River Coal Gasification Repowering Project (Wabash River Coal Gasification Repowering Project Joint Venture)	West Terre Haute, IN
Self-Scrubbing Coal™: An Integrated Approach to Clean Air (Custom Coals International)	Central City, PA
CCT-V	
Clean Coal Diesel Demonstration Project (Arthur D. Little, Inc.)	Fairbanks, AK
Clean Power from Integrated Coal/Ore Reduction (CPICOR™) (CPICOR™ Management Company, L.L.C.)	Vineyard, UT
Clean Energy Demonstration Project (Clean Energy Partners Limited Partnership)	Carbondale, IL
McIntosh Unit 4B Topped PCFB Demonstration Project (City of Lakeland, Lakeland Electric)	Lakeland, FL

Exhibit 2-3
Geographic Locations of CCT Projects—Environmental Control Devices

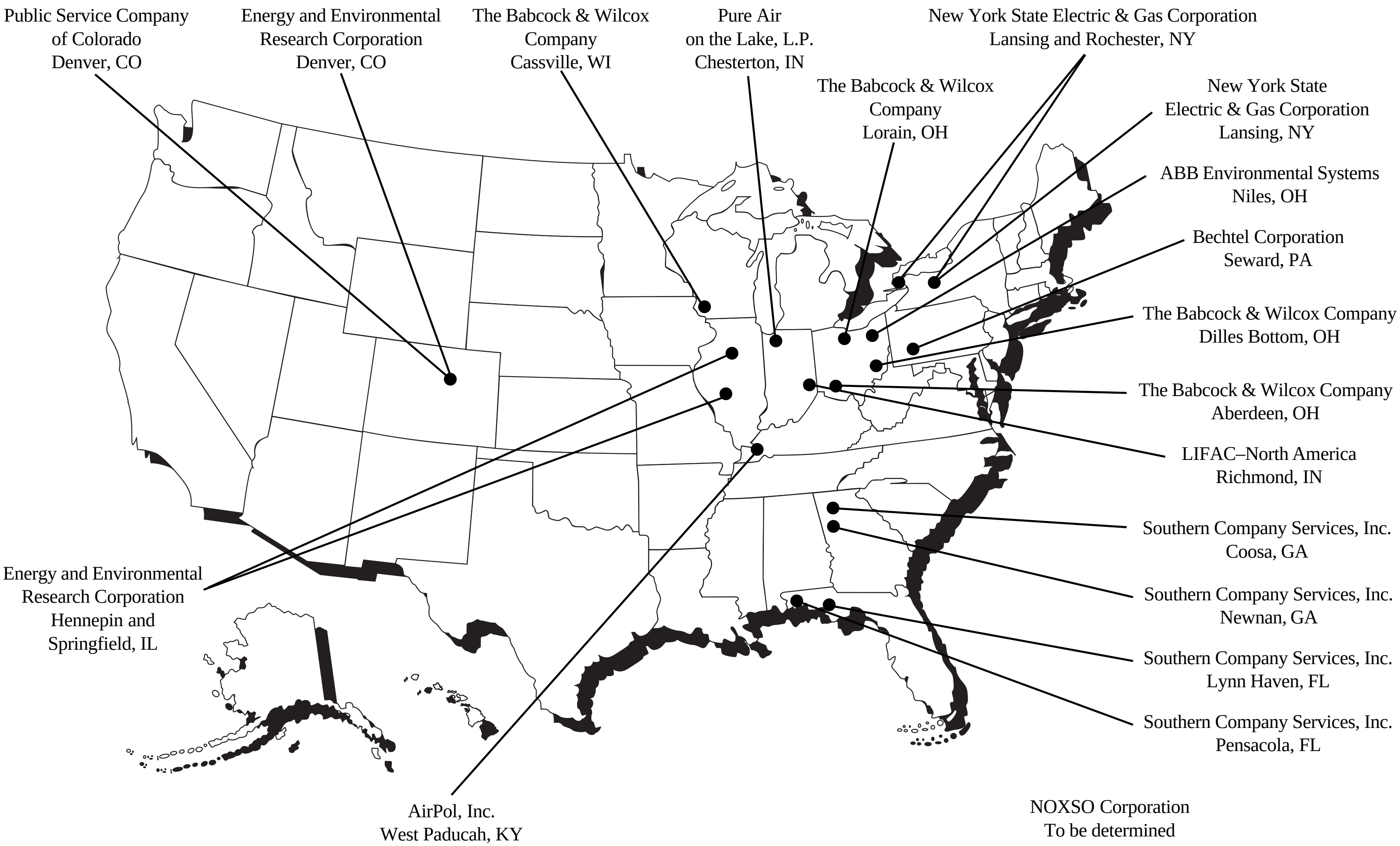


Exhibit 2-4

Geographic Locations of CCT Projects—Advanced Electric Power Generation

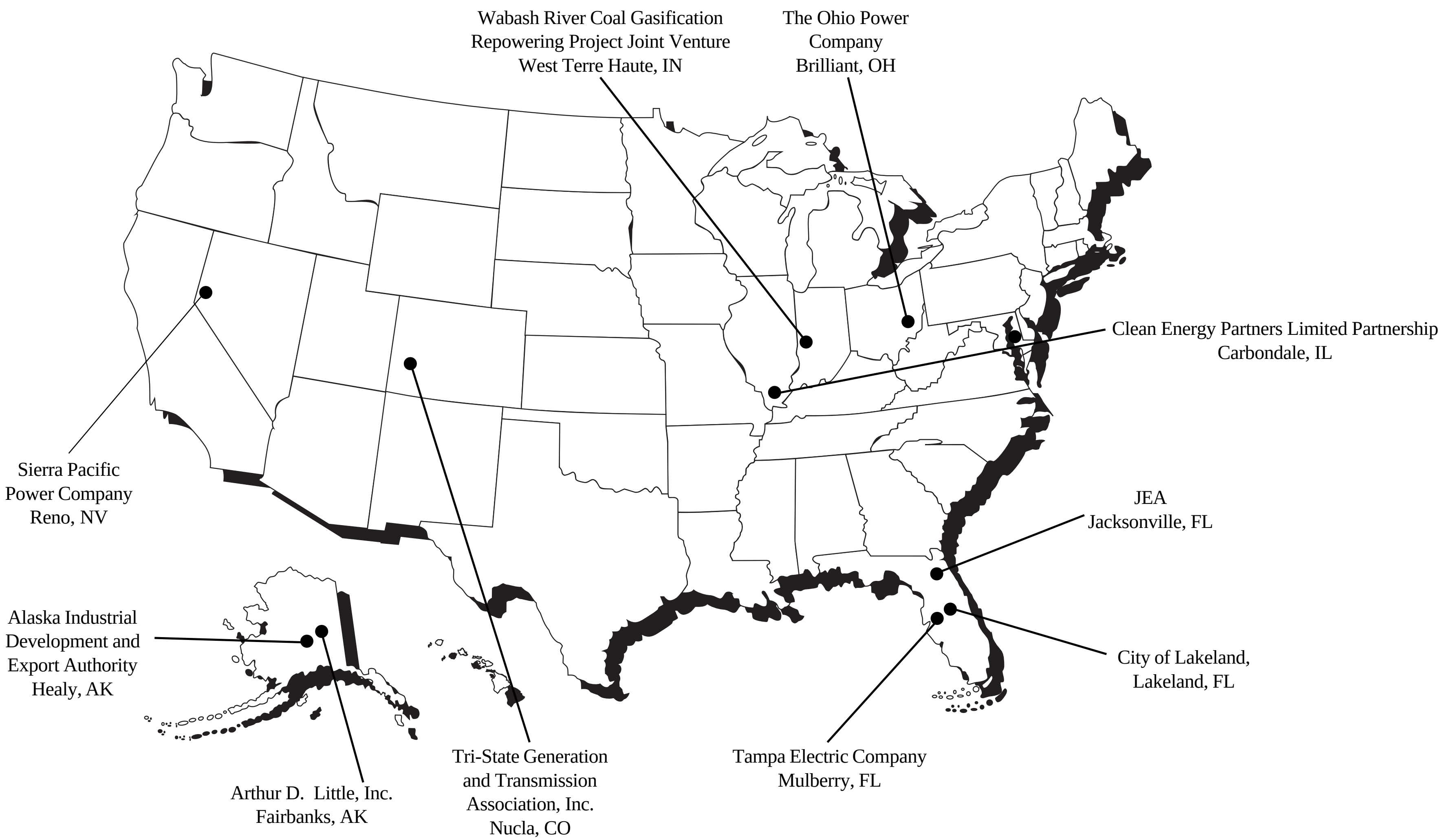


Exhibit 2-5
Geographic Locations of CCT Projects—Coal Processing for Clean Fuels

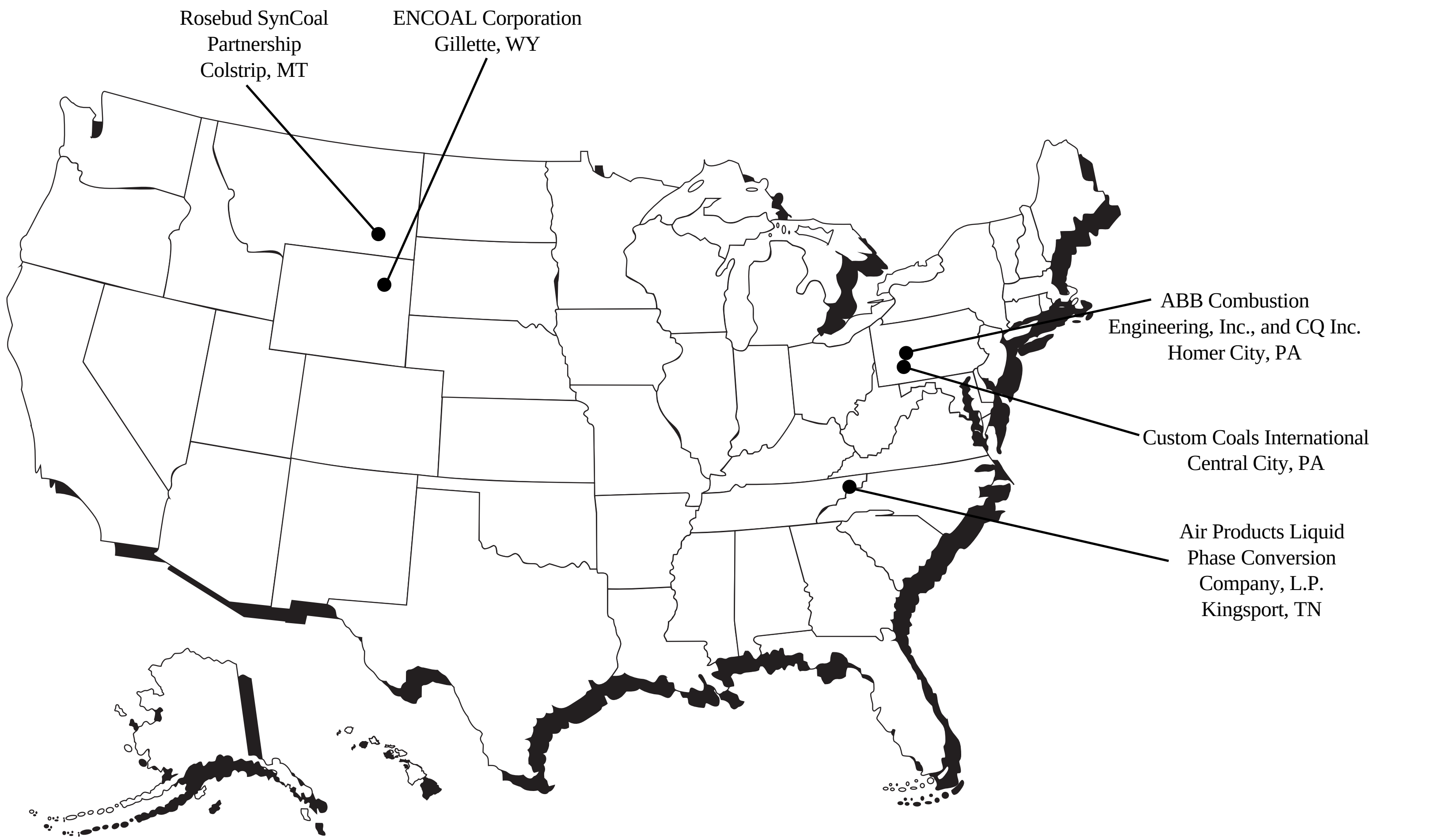


Exhibit 2-6
Geographic Locations of CCT Projects—Industrial Applications

MWe, approximately 25 percent of U.S. capacity, and consume about 36 percent of the coal produced domestically. Also participating were over 50 companies supplying technology and 30 providing engineering, construction, and consulting services.

The contributions of the selected projects to domestic and international energy and environmental needs are significant. These contributions include:

- Completing demonstration and proving commercial viability of a suite of cost-effective SO_2 and NO_x control options capable of achieving moderate (50 percent) to deep emission reduction (70–95 percent) for the full range of coal-fired boiler types;
- Providing the data base and operating experience requisite to making atmospheric fluidized-bed combustion a commercial technology at utility scale;
- Completing demonstration of a number of coal processes to produce high-energy-density, low-sulfur solid fuels and clean liquids from a range of coal types;
- Laying the foundation for the next generation of technologies to meet the energy and environmental demands of the 21st century—three IGCC plants in operation at three separate utilities; and demonstration of pressurized fluidized-bed combustion at 70 MWe successfully completed and two larger scale demonstrations in progress; and
- Demonstrating significant efficiency and pollutant emission reduction enhancements in steelmaking, advanced combustion for combined SO_2/NO_x/PM control for industrial and small utility boilers, and innovative SO_2 control for waste elimination in cement production.

Future Implementation Direction

The future implementation direction of the CCT Program focuses on completing the existing projects as promptly as possible and assuring the collection, analyses, and reporting of the operational, economic, and environmental performance results that are needed to affect commercialization.

In FY1999, the Clean Coal Diesel Demonstration Project is scheduled to begin operation and the following projects are forecasted to complete operations:

- Micronized Coal Reburning Demonstration for NO_x Control;
- Healy Clean Coal Project;
- Wabash River Coal Gasification Repowering Project;
- Advanced Coal Conversion Process Demonstration; and
- Blast Furnace Granular-Coal Injection System Demonstration.

The body of knowledge obtained as a result of the CCT Program demonstrations is being used in immediate decisionmaking relative to regulatory compliance, forging plans for meeting future energy and environmental demands, and developing the next generation of technology responsive to ever increasing demands on environmental performance at competitive costs. An expanded portfolio of information will be forthcoming to make it easier for stakeholders and customers to sift through the already enormous amount of data resulting from the demonstrations.

Efforts will continue toward refining the effectiveness in responding to customer and stakeholder needs. Toward that end, as needs change, forums will be sought to obtain feedback particularly in view of utility restructuring, continued environmental concerns, and a burgeoning foreign market. Objectives are to ensure that CCT Program efforts are fully leveraged and that follow-on efforts under the Office of Coal and Power Systems (OC&PS) RD&D Program are appropriate.

Three major drivers will affect implementation of the CCT Program because of the impact on market entry and deployment of the CCTs—environmental concerns, utility restructuring, and burgeoning demands for power in developing countries.

Environmental concerns. Perhaps the most immediate environmental concern relates to relieving seasonal ozone emissions in “ozone nonattainment areas.” To do so, EPA issued an ozone transport rule that requires major cuts in NO_x emissions in 22 states and the District of Columbia by 2003 (see page 1-6). Technologies and the associated databases developed under the CCT Program will play a role in responding to this requirement.

Increasing concerns over airborne particulate matter (PM) in the respirable range resulted in standards for particles 2.5 microns or less in size. Previous standards addressed airborne particles in the inhalable size range of 10 microns (about the size of bacteria) or less. But it is the respirable particles, $PM_{2.5}$, that can lodge in the lungs. $PM_{2.5}$ standards will not only require high PM capture efficiency, but also may put further pressure on SO_2 emission reduction. Sulfur compounds in the $PM_{2.5}$ range can be precipitated by SO_2 in stack gases.

Reduction of CO_2 in response to concerns over global climate change has been a major driver for the CCT Program. However, mandated CO_2 reduction as proposed in the Kyoto Protocol could impede coal-based power as an option for meeting new domestic demands for increased electric power generation for the foreseeable future. Provisions for trading CO_2 emissions between the United States and developing countries would mitigate pressure on domestic coal-based power. But such provisions were not a part of the Kyoto Protocol and remain in negotiation. Trading CO_2 emissions between the United States and developing countries would also provide a needed incentive for incremental investments for the more efficient CCTs in developing countries. Continued pressure to reduce CO_2 emissions has resulted in a new surge of research and development into CO_2 capture and sequestration. Advanced electric power generation technologies such as IGCC lend themselves to CO_2 capture. Therefore, progress in CO_2 capture and sequestration would serve to enhance IGCC marketability.

Utility Restructuring. Restructuring of the retail electric power generation portion of the utility sector from a regulated industry to a market-based industry has significant ramifications for CCTs domestically. It places pressure on the new technologies to not only have competitive costs but to have acceptable risk. No longer will risk and cost be born by the ratepayer. Under restructuring, the ratepayer becomes a conventional consumer looking for the best deal. Market niches may be found domestically, e.g., where multiple commodities are required and disadvantaged fuels can be used (e.g., IGCC using petroleum coke or biomass to produce electricity and fuels or chemicals). But the primary market for CCTs at least through 2005 will be developing countries, and more specifically, the Asian market. It is in the foreign markets where CCTs will realize significant commercialization and the associated reduction in cost and risk.

International Market. The market for CCTs in other parts of the world has tremendous near-term potential. For many countries, coal is the primary indigenous fuel and jobs and mitigation of poverty override the stigma attached to coal because of global climate change concerns. The total world power market between now and 2010 is estimated to be 950 GW. Of that total 50 percent resides in Asia, 30 percent in Europe, and 20 percent in the Americas. Within Asia, China alone has 16 percent of the total market, Japan/Indonesia/Korea have 17 percent and India alone 6 percent. These numbers plus reliance on coal in the Asian market make it the primary target for CCTs.

Realizing market potential for CCTs requires action to mitigate the higher risk and cost of CCTs. Project developers can seek cost saving measures such as use of disadvantaged fuels, production of multiple commodities, and firm definition of projects to reduce contingencies. Trading mechanisms for CO_2 such as the 161-nation “Global Environmental Facility” and others proposed hold promise for obtaining the incremental cost decreases for CCTs, assuming CO_2 reduction requirements or incentives are formalized.

Fluidized-bed combustion technology, the most mature CCT power system technology, has made inroads into foreign markets because of its tremendous fuel flexibility and proven track record. IGCC is realizing market penetration through use of disadvantaged fuels and production of multiple commodities. There are some 20 known IGCC projects worldwide, 10 already in place and 10 more in the planning stage.

3. Funding and Costs

Introduction

Congress has appropriated a federal budget of $2.3 billion for the CCT Program. These funds have been committed to demonstration projects selected through five competitive solicitations. As of September 30, 1998, the program consisted of 40 active or completed projects.

These 40 projects have resulted in a combined commitment by the federal government and the private sector of more than $5.6 billion. DOE's cost-share for these projects exceeds $1.9 billion, or approximately 34 percent of the total. The project participants (i.e., the non-federal-government participants) are providing the remaining $3.7 billion, or 66 percent of the total. Exhibit 3-1 summarizes the total costs of CCT projects as well as cost-sharing by DOE and project participants.

Program Funding

General Provisions

In the CCT Program, the federal government's contribution can not exceed 50 percent of the total cost of any individual project. The federal governments funding commitments and other terms of federal assistance are represented in a cooperative agreement negotiated for each project in the program. Terms of the cooperative agreement also include a plan for the federal government to recoup up to the full amount of the federal government's contribution. This approach enables taxpayers to benefit from commercially successful projects. This is in addition to the benefits derived from the demonstration and commercial deployment of technologies that improve environmental quality and promote the efficient use of the nation's coal resources.

The project participant has primary responsibility for the project. The federal government monitors project activities, provides technical advice, and assesses progress by periodically reviewing project

Exhibit 3-1
CCT Project Costs and Cost-Sharing
(Dollars in Thousands)

	Total Project Costs	%	Cost-Share DOE[b]	Cost-Share Participants	Percent DOE	Percent Participants
Subprogram						
CCT-I	730,920	13	239,645	491,275	33	67
CCT-II	319,177	6	139,520	179,657	44	56
CCT-III	1,409,387	25	618,947	790,440	44	56
CCT-IV	1,037,815	18	477,058	560,757	46	54
CCT-V	2,174,173	38	466,196	1,707,977	21	79
Total[a]	5,671,472	100	1,941,365	3,730,106	34	66
Application Category						
Advanced Electric Power Generation	3,159,911	56	1,224,078	1,935,832	39	61
Environmental Control Devices	704,862	12	295,191	409,670	42	58
Coal Processing for Clean Fuels	519,196	9	230,024	289,172	44	56
Industrial Applications	1,287,503	23	192,072	1,095,431	15	85
Total[a]	5,671,472	100	1,941,365	3,730,106	34	66

[a] Totals may not add due to rounding.

[b] DOE share does not include $52,512,231 obligated for withdrawn, terminated, and concluded projects.

Exhibit 3-2
Relationship between Appropriations and Subprogram Budgets for the CCT Program
(Dollars in Thousands)

Appropriation Enacted	Subprogram	Adjusted Appropriations	SBIR & STTR Budgets[a]	Program Direction Budget	Projects Budget
P.L. 99-190	CCT-I	380,600	4,902	72,467	303,231
P.L. 100-202	CCT-II	473,997	6,781	32,512	434,704
P.L. 100-446	CCT-III	574,998	6,906	22,548	545,544
P.L. 101-121[b]	CCT-IV	427,000	7,065	25,000	394,935
P.L. 101-121[b]	CCT-V	450,000	5,427	25,000	419,573
Total		2,306,595	31,081	177,527	2,097,987

[a] Small Business Innovation Research (SBIR) and Small Business Technology Transfer (STTR) Programs.

[b] P.L. 101-121 was revised by P.L. 101-512, 102-154, 102-381, 103-138, 103-332, 104-6, 104-208, 105-18, 105-83, and 105-277.

performance with the participant. The federal government also participates in decision making at major project junctures negotiated into the cooperative agreement. Through these activities, the federal government ensures the efficient use of public funds in the achievement of individual project and overall program objectives.

Congress has provided program funding through appropriation acts and adjustments. (See Appendix A for legislative history and excerpts from the relevant funding legislation.)

Exhibit 3-2 presents the allocation of appropriated CCT Program funds (after adjustment) and the amount available for each CCT solicitation. Additional activities funded by CCT Program appropriations are the Small Business Innovation Research (SBIR) Program, the Small Business Technology Transfer (STTR) Program, and CCT Program direction. The SBIR Program implements the Small Business Innovation Development Act of 1982 and provides a role for small, innovative firms in selected research and development (R&D) areas. The STTR Program implements the Small Business Technology Transfer Act of 1992 that establishes a pilot program and funding for small business concerns performing cooperative R&D efforts.

The CCT program direction budget provides for the management and administrative costs of the program and includes federal employees' salaries, benefits and travel, site support services, and services provided by national laboratories and private firms.

Availability of Funding

Although all funds necessary to implement the entire CCT Program were appropriated by Congress prior to FY1990, the legislation also directed that these funds be made available (i.e., apportioned) to DOE on a time-phased basis. Exhibit 3-3 depicts this apportionment of funding to DOE. Exhibit 3-3 also shows the program's yearly funding profile by appropriations act and by subprogram. Funds can be transferred among subprogram budgets to meet project and program needs.

Use of Appropriated Funds

There are five key financial terms used by the government to track the status and use of appropriated funds: (1) budget authority, (2) commitments, (3) obligations, (4) costs, and (5) expenditures. The definition of each of these terms is described below.

- **Budget Authority.** This is the legal authorization created by legislation (i.e., an appropriations act) that permits the federal government to obligate funds.
- **Commitments.** Within the context of the CCT Program, a commitment is established when DOE selects a project for negotiation. The commitment amount is equal to DOE's share of the project costs contained in the cooperative agreement.
- **Obligations.** The cooperative agreement for each project establishes funding increments, referred to as budget periods. The cooperative agreement defines the tasks to be performed in each budget period. An obligation occurs in the beginning of each budget period and establishes the incremental amount of federal funds

Exhibit 3-3
Annual CCT Program Funding by Appropriations and Subprogram Budgets
(Dollars in Thousands)

Fiscal Year	1986–90	1991	1992	1993	1994	1995	1996	1997	1998	1999	2000-02[e]	Total[d]
Adjusted Appropriations[a]												
P.L. 99-190	397,600							(17,000)				380,600
P.L. 100-202	375,000	199,997							(101,000)	(40,000)	40,000	473,997
P.L. 100-446	419,000	155,998										574,998
P.L. 101-121[b]		35,000	315,000	0	100,000	18,000	50,000	(91,000)				427,000
P.L. 101-121[b]			100,000	0	125,000	19,121	100,000	105,879				450,000
Total	1,191,600	390,995	415,000	0	225,000	37,121	150,000	(2,121)	(101,000)	(40,000)	40,000	2,306,595
Subprogram Budgets												
CCT-I Projects	387,231					(18,000)	(18,000)	(33,000)	(15,000)	(14,900)		288,331
CCT-II Projects	338,207	197,497							(101,000)	(40,000)	40,000	434,704
CCT-III Projects	391,496	154,048										545,544
CCT-IV Projects		9,875	311,063	0	98,450	17,622	48,925	(91,000)				394,935
CCT-V Projects			74,062	0	123,063	18,719	97,850	105,879				419,573
Projects Subtotal	1,116,934	361,420	385,125	0	221,513	18,341	128,775	(18,121)	(116,000)	(54,900)	40,000	2,083,087
Program Direction	60,527	25,000	25,000			18,000	18,000	16,000	15,000	14,900		192,427
Fossil Energy Subtotal	1,177,461	386,420	410,125	0	221,513	36,341	146,775	(2,121)	(101,000)	(40,000)	40,000	2,275,514
SBIR & STTR[c]	14,139	4,575	4,875	0	3,487	779	3,225					31,081
DOE Total[d]	1,191,600	390,995	415,000	0	225,000	37,121	150,000	(2,121)	(101,000)	(40,000)	40,000	2,306,595

[a] Shown are appropriations less amounts sequestered under the Gramm-Rudman-Hollings Deficit Reduction Act.

[b] Shown is the fiscal year apportionment schedule of P.L. 101-121 as revised by P.L. 101-512, 102-154, 102-381, 103-138, 103-332, 104-6, 104-208, 105-18, 105-83, and 105-277.

[c] Small Business Innovation Research (SBIR) and Small Business Technology Transfer (STTR) Programs.

[d] Totals may not appear to add due to rounding.

[e] P.L. 105-277 deferred the availability of $40 million in FY1999. Availability of the funds are to be restored in FY2000 through FY2002 in increments of $10, $15, and $15 million.

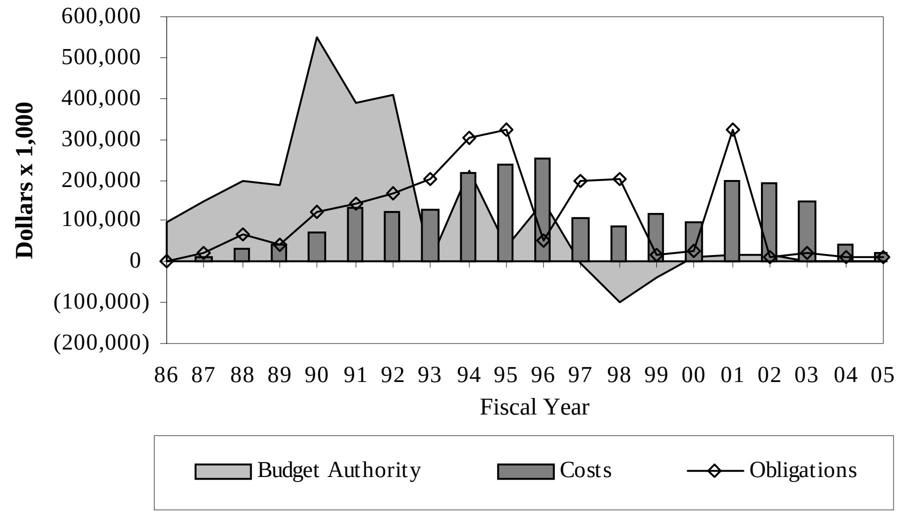
available to the participant for use in performing tasks as defined in the cooperative agreement.

- **Costs.** A request for payment submitted by the project participant to the federal government for reimbursement of tasks performed under the terms of the cooperative agreement is considered a cost. Costs are equivalent to a bill for payment or invoice.
- **Expenditures.** Expenditures represent payment amounts to the project participant from checks drawn upon the U.S. Treasury.

The full government cost-share specified in the cooperative agreement is considered committed to each project. However, DOE obligates funds for the project in increments. Most projects are subdivided into several time and funding intervals, or budget periods. The number of budget periods is determined during negotiations and is incorporated into the cooperative agreement. DOE obligates sufficient funds at the beginning of each budget period to cover the government's cost-share for that period. This procedure limits the government's financial exposure and assures that DOE fully participates in the decision to proceed with each major phase of project implementation.

The overall financial profile for the CCT Program is presented in Exhibit 3-4. The graph shows actual performance for FY1986 through FY1998 and DOE estimates for FY1999 through program completion. Excluded from the graph are SBIR and STTR funds, as these are used and tracked separately from the CCT Program. The financial projections presented in Exhibit 3-4 are based on individual project schedules and budget periods as defined in the cooperative agreements and modifications. The negative Budget Authority values shown in Exhibit 3-4 for fiscal years 1998 and 1999 result from rescission of $101 million in FY1998 and the deferral of $40 million in FY1999.

Exhibit 3-4
CCT Financial Projections as of September 30, 1998



The financial status of the program through September 30, 1998, is presented by subprogram in Exhibit 3-5. SBIR and STTR funds are included in this exhibit to account for all funding. Exhibit 3-5 also indicates the apportionment sequence as modified by Public Law 105-277. These values represent the amount of budget authority available for the CCT Program.

Project Funding, Costs, and Schedules

Information for individual CCT projects, including funding and the status of key milestones, is provided in Section 5. An overview of project schedules and funding is presented in Exhibit 3-6.

Cost-Sharing

A characteristic feature of the CCT Program is the cooperative funding agreement between the participant and the federal government referred to as cost-sharing. This cost-sharing approach, as implemented in the CCT Program, was introduced in Public Law 99-190, An Act Making Appropriations for the Department of the Interior and Related Agencies for the Fiscal Year Ending September 30, 1986, and for Other Purposes. General concepts and requirements of the cost-sharing principle as applied to the CCT Program include the following elements:

- The federal government may not finance more than 50 percent of the total costs of a project;

Exhibit 3-5
Financial Status of the CCT Program as of September 30, 1998
(Dollars in Thousands)

Subprogram	Appropriations Allocated to Subprogram[b]	Apportioned to Date[c]	Committed to Date	Obligated to Date	Cost to Date
CCT-I	303,231	303,231	257,157	257,157	183,885
CCT-II	434,704	394,704	171,489	172,317	165,499
CCT-III	545,544	545,544	618,947	618,684	451,201
CCT-IV	394,935	394,935	477,889	477,889	457,621
CCT-V	419,573	419,573	468,396	148,331	10,169
Projects Subtotal	2,097,987	2,057,987	1,993,878	1,674,378	1,268,375
SBIR & STTR[a]	31,081	31,081	31,081	31,081	31,081
Program Direction	177,527	177,527	177,527	174,584	171,336
Total	2,306,595	2,266,595	2,202,486	1,880,043	1,470,792

[a] Small Business Innovation Research (SBIR) and Small Business Technology Transfer (STTR) Programs

[b] Totals may not appear to add due to rounding.

[c] Reflects $40 million deferral required by P.L. 105-277.

Apportionment Sequence

FY	Annual	Cumulative
1986	99,400	99,400
1987	149,100	248,500
1988	199,100	447,600
1989	190,000	637,600
1990	554,000	1,191,600
1991	390,995	1,582,595
1992	415,000	1,997,595
1993	0	1,997,595
1994	225,000	2,222,595
1995	37,121	2,259,716
1996	150,000	2,409,716
1997	(2,121)	2,407,595
1998	(101,000)	2,306,595
1999	(40,000)	2,266,595
2000	10,000	2,276,595
2001	15,000	2,291,595
2002	15,000	2,306,595

- Cost-sharing by the project participants is required throughout the project (design, construction, and operation);
- The federal government may share in project cost growth (within the scope of work defined in the original cooperative agreement) up to 25 percent of the originally negotiated government share of the project;
- The participant's cost-sharing contribution must occur as project expenses are incurred and cannot be offset or delayed based on prospective project revenues, proceeds, or royalties; and
- Investment in existing facilities, equipment, or previously expended R&D funds are not allowed for the purpose of cost-sharing.

As previously discussed, Exhibit 3-1 summarizes the cost-sharing status by subprogram and by application category for the 40 active or completed projects. In the advanced electric power generation category, which accounts for 56 percent of total project costs, participants are contributing 61 percent of the funds. Cost-sharing by participants for environmental control devices, coal processing for clean fuels, and industrial

Exhibit 3-6
CCT Project Schedules and Funding, by Application Category

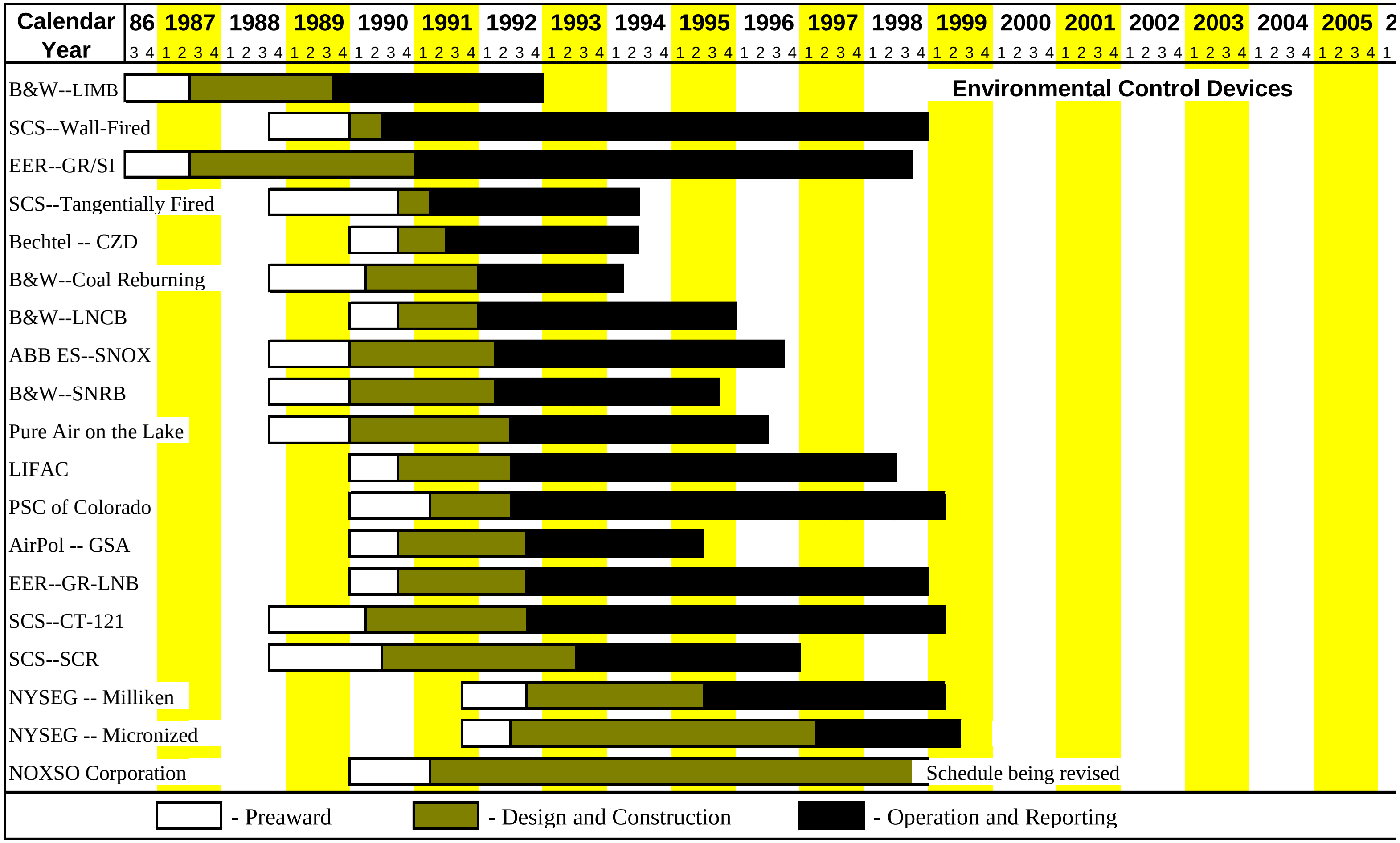
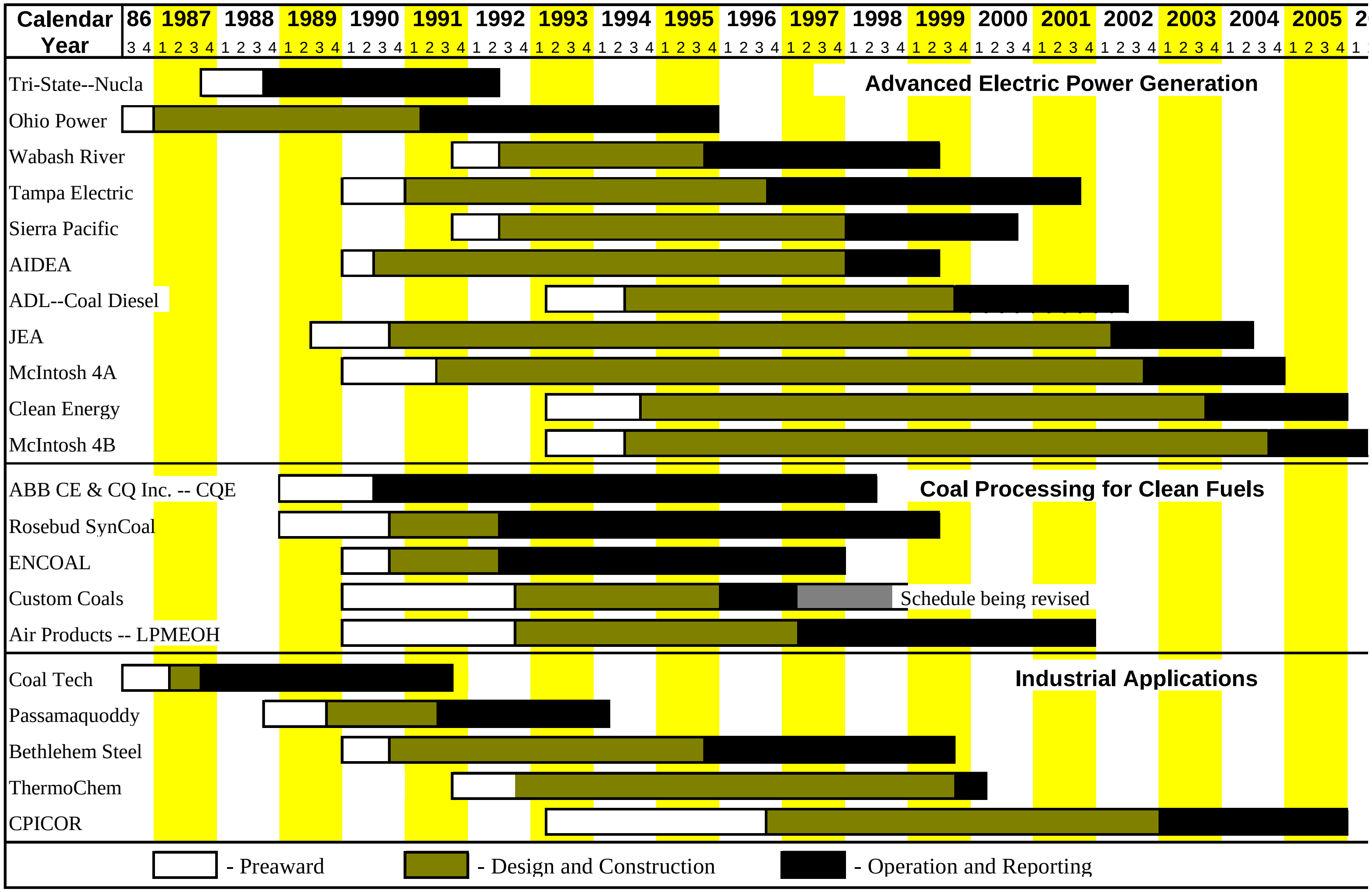


Exhibit 3-6 (continued)
CCT Project Schedules and Funding, by Application Category



applications categories is 58 percent, 56 percent, and 85 percent, respectively. For the overall program, participants are contributing 66 percent of the total funding, or $1.79 billion more than the federal government.

Recovery of Government Outlays (Recoupment)

The policy objective of DOE is to recover an amount up to the government's financial contribution to each project. Participants are required to submit a plan outlining a proposed schedule for recovering the government's financial contribution. The solicitations have featured different sets of recoupment rules.

Under the first solicitation, repayment was derived from revenue streams that include net revenue from operation of the demonstration plant beyond the demonstration phase and the commercial sale, lease, manufacture, licensing, or use of the demonstrated technology. In CCT-II, repayment was limited to revenues realized from the future commercialization of the demonstrated technology. The government's share would be 2 percent of gross equipment sales and 3 percent of the royalties realized on the technology subsequent to the demonstration.

The CCT-III repayment formula was adjusted to 0.5 percent of equipment sales and 5 percent of royalties. Limited grace periods were allowed on a project-by-project basis. A waiver on repayment may be sought from the Secretary of Energy if the project participant determines that a competitive disadvantage would result in either the domestic or international marketplace.

The recoupment provisions for CCT-IV and CCT-V were identical to those in CCT-III.

As of September 30, 1998, five projects have made repayments to the federal government: Nucla CFB Demonstration Project (Tri-State Generation and Transmission Association, Inc.); Full-Scale Demonstration of Low-NO_x Cell Burner Retrofit (The Babcock & Wilcox Company); Development of the Coal Quality Expert™ (ABB Combustion Engineering, Inc., and CQ Inc.); 10-MWe Demonstration of Gas Suspension Absorption (AirPol, Inc.); and the Advanced Flue Gas Desulfurization Demonstration Project (Pure Air on the Lake, L.P.).

In September 1997, the CCT Program office issued a report entitled *Recoupment Lessons Learned-Clean Coal Technology Demonstration Program*. The report: (1) reviewed the lessons learned on "recoupment" during the implementation of the CCT Program; (2) addressed recommended actions set forth in General Accounting Office (GAO) Report RCED-92-17, GAO Report RCED-96-141, and Inspector General Audit Report IG-0391 relative to "recoupment;" and (3) provided input into DOE deliberations on "recoupment" policy.

4. CCT Program Accomplishments

Introduction

The success of the CCT Program ultimately will be measured by the contribution the technologies make to the resolution of energy, economic, and environmental issues. These contributions can only be achieved if the public and private sectors understand that clean coal technologies can increase the efficiency of energy use and enhance environmental quality at costs that are competitive with alternative energy options.

The CCT Program has continued efforts to define and understand the potential domestic and international markets for clean coal technologies. Domestically, this activity requires a continuing dialogue with electric utility executives, public utility commissioners, and financial institutions. Also required are analyses of the effect that regional electric capacity requirements, environmental compliance strategies, and electric utility restructuring have on the demand for clean coal technologies. Internationally, activities include participating in international conferences and workshops, furnishing information on clean coal technologies, and providing technical support to trade agencies, trade missions, and financial organizations.

The following projects completed operation during fiscal year 1998:

- Demonstration of Advanced Combustion Techniques for a Wall-Fired Boiler; and
- Milliken Clean Coal Technology Demonstration Project.

Throughout the 1998 fiscal year, the CCT Program staff participated in over 15 domestic and international events involving users and vendors of clean coal technologies, regulators, financiers, environmental groups, and other public and private institutions. Included was the Sixth Annual Clean Coal Technology Conference, held in Reno, Nevada and attended by 340 participants from 22 countries. Four issues of the *Clean Coal Today* newsletter were published in the same period, along with the third annual edition of the *Clean Coal Today Index*, which cross-references all articles published in the newsletter. Publication of the second *Clean Coal Technology Program Bibliography of Publications, Papers, and Presentations* highlighted efforts to document the progress and results of the demonstration projects. The DOE also continued expanded coverage of the program by publishing the *Clean Coal Technology Demonstration Program: Update 1996-97*, and the mid-year update of project factsheets, *Clean Coal Technology Demonstration Program: Project Fact Sheets 1997*.

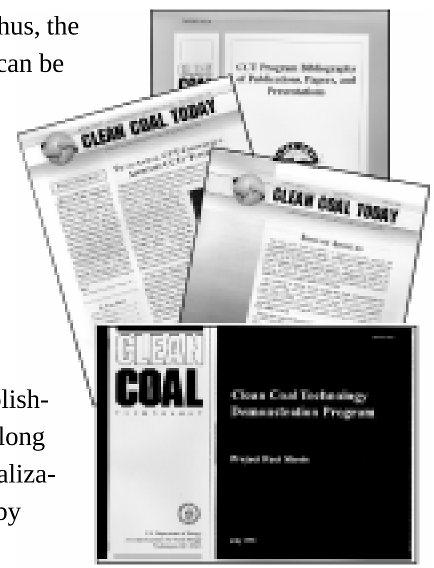
Marketplace Commitment

Reflecting CCT Program commercialization goals, the majority of the projects involve demonstrations at commercial scale, providing the opportunity for the participants to continue operation of the demonstrated technologies as part of their strategy to comply with the CAAA.

With government serving as a risk-sharing partner, industry funding has been leveraged to:

- Create jobs,
- Improve the environment,
- Reduce the cost of compliance with environmental regulations,
- Reduce the cost of electricity generation,
- Improve power generation efficiencies, and
- Position U.S.-based industry to export innovative services and equipment.

Reflecting the marketplace commitment, the CCT projects are organized within four major product markets—environmental control devices, advanced electric power generation, coal processing for clean fuels, and industrial applications. Thus, the CCT Program can be viewed from a market perspective. This section of the *Program Update* highlights some of the program and project accomplishments to date along with commercialization successes by market sector.



Environmental Control Devices

Control of SO_2 and NO_x emissions from existing coal-fired boilers was the initial thrust of the program; thus, 17 of the 19 environmental control device projects have now completed operations. The completed demonstrations proved commercial viability of a suite of cost-effective SO_2 and NO_x control options for the full range of coal-fired boiler types. Risk was significantly mitigated in successfully applying the technologies commercially because of the extensive databases and attendant predictive models developed through the demonstrations. Also, projects were leveraged to provide input in formulating NO_x control requirements under the CAAA and to evaluate the impact of emerging issues, such as air toxics, on the existing boiler population and control options. Extensive air toxics testing was performed in conjunction with 10 of the environmental control projects. To a great extent, the technologies were retained for commercial service at the demonstration sites and many technology suppliers have realized commercial sales.

SO_2 Control Technologies. All five SO_2 control technology demonstrations have completed operations, evaluating three basic approaches to address the diverse coal-fired boiler population:

- Two low-capital cost **sorbent injection** systems, sponsored by LIFAC–North America and Bechtel Corporation, demonstrated SO_2 capture efficiencies in the range of 50 to 70 percent. These systems hold particular promise for the older, smaller units, particularly those with space constraints.
- A moderate-capital cost **gas-suspension-absorption** system, sponsored by AirPol, Inc., demonstrated SO_2 capture efficiencies in the range of 60 to 90 percent. The system has particular applicability to the small- to mid-range units with some space limitations.
- Two **advanced flue gas desulfurization** (AFGD) systems, sponsored by Pure Air on the Lake, L.P. and Southern Company Services, having somewhat higher capital costs than the other approaches, demonstrated SO_2 capture efficiencies in the range of 90 to 95 percent. These systems are primarily applicable to the larger, newer units that have space available.

The AFGD projects redefined the state-of-the technology by proving that a single absorber module of advanced design could process large volumes of flue gas and provide the required availability and reliability. This single module design, without the usual spares, combined with integration of functions within the absorber module and use of high throughput designs, significantly reduced capital cost and space requirements. The AFGD testing also established that wallboard-grade gypsum could be produced in lieu of solid waste; wastewater discharge could be eliminated; and, by mitigating corrosion, fiberglass-reinforced-plastic fabrication could eliminate process steps (e.g., pre-quenching for chloride removal and flue gas reheat).

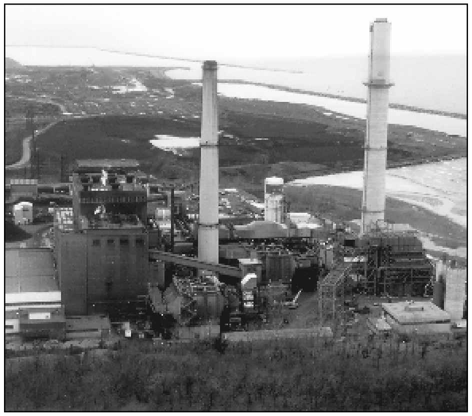
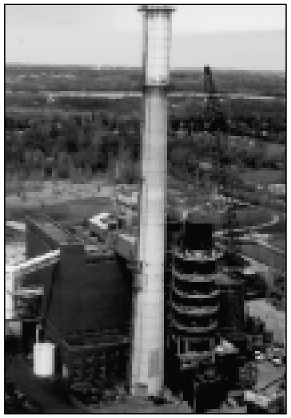
The AFGD demonstration by Southern Company Services using Chiyoda CT-121 showed that the system could significantly enhance particulate control. Pure Air on the Lake, L.P., introduced an innovative business concept whereby the company builds, owns, and operates scrubbers as a contracted service to a utility. The arrangement relieves utilities of the burden of ownership and operation and has proven to be an attractive approach.

Commercialization successes to date for the SO_2 control technologies are summarized in Exhibit 4-1.

NO_x Control Technology. Six of the seven NO_x control technology demonstrations have successfully completed operations. Testing was conducted on the four major boiler types (wall-fired, tangentially-fired, cyclone-fired, and cell-burner boilers), representing over 90 percent of the coal-fired boiler population; however, applicability extends to all boiler types.

Typically, NO_x emission reductions achieved for the various approaches were:

▼ SO_2 control technologies: AirPol (left), Pure Air (center), and LIFAC (right).

- Low NO_x burners: 45 to 63 percent
- Reburning systems: 50 to 67 percent
- SNCR systems: 30 to 50 percent
- SCR systems: 80 to 90+ percent
- Advanced controls: 10 to 15 percent

The database developed during Southern Company Services' evaluation of NO_x control on wall-fired and tangentially-fired boilers at Plant Smith and Plant Hammond, respectively, was used by the Environmental Protection Agency (EPA) in formulating NO_x provisions under the CAAA. Babcock & Wilcox's low NO_x burner systems, ABB Combustion Engineering's LNCFS™ for tangentially-fired boilers, and Foster Wheeler's low NO_x burner system for wall-fired boilers have realized commercial acceptance.

The Babcock & Wilcox Company's low NO_x cell burner, LNCB™, provided an effective low-cost plug-in NO_x control system for cell-burner boilers, which are known for their inherently high NO_x emissions.

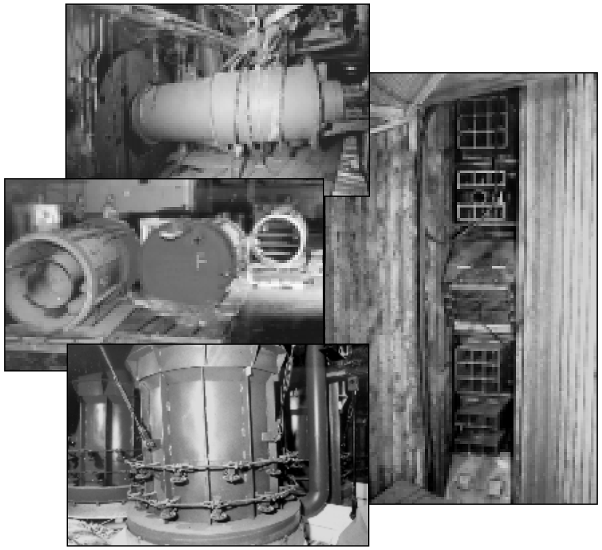
Integration of neural-network systems into digital boiler controls, such as the Generic NO_x Control Intelligence System (GNOCIS) installed at Plant Hammond, demonstrated effective optimization of parameters for NO_x control and boiler performance under load-following operations.

The Babcock & Wilcox Company's coal reburning technology proved not only to be an effective way to control NO_x on cyclone boilers, but a means to avoid derating cyclone boilers when switching to low-sulfur, low-rank western coals. Energy and Environmental Research Corporation's use of gas reburning, applicable to all boiler types, introduced an alternative to SCR for high NO_x emission reduction particularly when used with low NO_x burners.

In another project, comparative analyses were conducted on a range of SCR catalysts operated on high-sulfur U.S. coals, providing needed insight on the environmental and economic performance potential of SCR. Other SCR systems and selective non-catalytic

Exhibit 4-1
Commercial Successes—SO_2 Control Technology

Project and Participant	Commercialization Progress
LIFAC Sorbent Injection Desulfurization Demonstration Project (LIFAC–North America)	Technology retained for commercial use at host site First high-sulfur coal application 10 commercial units in operation or construction (Canada, China, Finland, Russia, and U.S.)
10-MWe Demonstration of Gas Suspension Absorption (AirPol, Inc.)	Sale of 50-MWe unit to city of Hamilton, OH – Value—$10 million Sale to U.S. Army for hazardous waste disposal – Value—$1.3 million Sale to Sweden for iron ore sinter plant (no value available) Sales to Taiwan and India – Combined value—$33 million Sale of technical assistance and proprietary equipment to Taiwan – Value—$1 million
Advanced Flue Gas Desulfurization Demonstration Project (Pure Air on the Lake, L.P.)	Technology retained for commercial use at host site; first scrubber to comply with CAAA installed; Wallboard manufacturer using all gypsum produced
Demonstration of Innovative Applications of Technology for the CT-121 FGD Process (Southern Company Services, Inc.)	Technology retained for commercial use at host site Since the CCT Program demonstration, over 8,200 MWe equivalent of CT-121 FGD capacity has been sold to 16 customers in seven countries



▲ Low NO_x burner technologies: Foster Wheeler's low NO_x burner for wall-fired boilers (top left), ABB Combustion Engineering's LNCFS™ for tangentially fired boilers (right), Babcock & Wilcox's LNCB® for cell-burner boilers (center), and Babcock & Wilcox's DRB-XCL® for down-fired boilers (bottom).

reduction (SNCR) systems were demonstrated on combined SO_2/NO_x control technologies.

Commercialization successes to date for the NO_x control technologies are summarized in Exhibit 4-2.

Combined SO_2/NO_x Control Technologies. Six of the seven combined SO_2/NO_x control technology demonstrations have successfully completed operations. The demonstrations tested a multiplicity of complementary and synergistic control methods to achieve cost-effective SO_2 and NO_x emissions reductions.

SNOX™, a catalytic process developed by Haldor Topsoe a/s, consistently achieved 95 and 94 percent SO_2 and NO_x control, respectively. The process also demonstrated excellent particulate control, while producing a salable by-product in lieu of solid waste.

In a project sponsored by Public Service Company of Colorado, complementary use of low NO_x burners with SNCR resulted in NO_x emission reductions of greater than 80 percent. SNCR interacted synergistically with sorbent injection to reduce ammonia slip and NO_2 emissions. Sodium-based sorbent injection achieved 70 percent SO_2 removal at high sorbent utilization rates.

New York State Electric and Gas (NYSEG) evaluated an advanced flue gas desulfurization system, the S-H-U scrubber process. The S-H-U process is an advanced formic acid-enhanced wet limestone scrubbing process that removes 98 percent of the SO_2 in the flue gas. In conjunction with the S-H-U- process, NYSEG also evaluated micronized coal as a reburn fuel using close coupled reburning techniques and deep staging over ABB Combustion Engineering, Inc.'s low NO_x burners. DHR Technologies supplied a plant optimization control system known as the Plant Emission Optimization Advisor or PEOA™, which has been sold to a number of users in the power industry.

The Babcock & Wilcox Company's SO_x-NO_x-Rox Box™, an integration of a newly developed high-temperature fabric-filter bag (for baghouse installation) with SCR and sorbent injection, proved to be an easily installed, highly efficient control system for SO_2, NO_x, and particulates. Typical performance was 80 percent SO_2 removal, 90 percent NO_x removal, and 99.9 percent particulate removal.

Limestone injection multistage burner (LIMB) and Coolside (duct injection of lime sorbents) demonstrations proved that sorbent injection methods could achieve up to 70 percent SO_2 reduction. The Babcock & Wilcox DRB-XCL® advanced low NO_x burners reduced NO_x emissions by 45 percent.

Energy and Environmental Research Corporation's demonstration of gas reburning and sorbent injection showed that NO_x reductions greater than 60 percent could be achieved with only 13 percent gas heat input. Furthermore, SO_2 removal of over 55 percent was achieved by using special sorbents.

NOXSO Corporation's demonstration of a dry, regenerable flue gas cleanup process is predicted to remove 98 percent of the SO_2 and 75 percent of the NO_x from a coal-fired boiler's flue gas.

Exhibit 4-2
Commercial Successes—NO_x Control Technology

Project and Participant	Commercialization Progress
Demonstration of Coal Reburning for Cyclone Boiler NO_x Control (The Babcock & Wilcox Company)	Technology retained for commercial use at host site
Full-Scale Demonstration of Low-NO_x Cell Burner Retrofit (The Babcock & Wilcox Company)	Technology retained for commercial use at host site Seven commercial contracts awarded for 144 burners – Value—$27 million
Evaluation of Gas Reburning and Low-NO_x Burners on a Wall-Fired Boiler (Energy and Environmental Research Corporation)	Technology retained for commercial use at host site
Demonstration of Advanced Combustion Techniques for a Wall-Fired Boiler (Southern Company Services, Inc.)	Technology retained for commercial use at host site Foster Wheeler has equipped 86 boilers with low NO_x technology (51 domestic and 35 international) – Quantity—1,800 burners for over 30,000 MWe capacity 19 GNOCIS neural-network control projects underway Expect another 17 GNOCIS projects in 1999 Organizations selected to market GNOCIS in U.S. and abroad
180-MWe Demonstration of Advanced Tangentially Fired Combustion Techniques (Southern Company Services, Inc.)	Technology retained for commercial use at host site ABB Combustion Engineering has modified 116 coal-fired tangentially-fired boilers, representing over 25,000 MWe, with LNCFS™ and TFS 2000™

Commercialization successes to date for the combined SO_2 and NO_x control technologies are summarized in Exhibit 4-3.

Advanced Electric Power Generation

Pollution control was the early priority in the CCT Program. But, technologies also were sought that could effectively repower aging plants faced with the need to install pollution controls and respond to growing power demands. Contributing to this search was the recognition that existing power generation sites had significant value and warranted investment, given the permitting problems associated with siting new plants. This recognition led to award early on of three key repowering projects—two atmospheric fluidized-bed combustion (ACFB) projects and a pressurized fluidized-bed combustion (PFBC) project.

Exhibit 4-3
Commercial Successes—Combined SO_2/NO_x Control Technology

Project and Participant	Commercialization Progress
SNOX™ Flue Gas Cleaning Demonstration Project (ABB Environmental Systems)	Technology retained for commercial use at host site 305 MWe unit operating in Denmark on coal 30 MWe unit operating in Sicily on petroleum coke
LIMB Demonstration Project Extension and Coolside Demonstration (The Babcock & Wilcox Company)	Sale of LIMB to independent power project in Canada
Enhancing the Use of Coals by Gas Reburning Sorbent Injection (Energy and Environmental Research Corporation)	Illinois Power retained gas reburning for commercial use City Water, Light & Power retained gas reburning for commercial use
Milliken Clean Coal Technology Demonstration Project (New York State Electric & Gas Corporation)	Four sales of DHR Technologies' Plant Emission Optimization Advisor More than 20 NO_x OUT® or NO_x OUT® derivative units sold in U.S, Taiwan, and Korea
	U.S. company, SHN, established to market S-H-U scrubber Actively pursuing AFGD bid for Pennsylvania site (will include S-H-U process, Stebbins absorber module, and heat-pipe air preheater)
Integrated Dry NO_x/SO_2 Emissions Control System (Public Service Company of Colorado)	Technology retained for commercial use at host site Sales of Babcock & Wilcox DRB-XCL® low-NO_x burners (which are components of the technology demonstrated) – Quantity—2,428 burners for 31,467 MWe capacity – Value—$320 million

As the CCT Program unfolded, a number of energy and environmental issues combined to change the emphasis toward seeking highly-efficient, very low-emission power generation technologies for both repowering and new power generation. This emphasis was deemed requisite to coal fulfilling its projected contribution to the nation's energy mix well into the 21st century. Environmental issues included a growing concern over greenhouse gas emissions. In addition, SO_2 emissions had been capped under the CAAA; NO_x continued to receive increased attention in ozone nonattainment areas; and fine particulate emissions (respirable dust) were identified as a particular health threat. These issues prompted follow-on projects in PFBC, initiation of projects in integrated gasification combined cycle (IGCC), and projects in advanced combustion and heat engines.

Fluidized-Bed Combustion. The Tri-State Generation and Transmission Association, Inc. Nucla Station repowering project provided the database and operating experience requisite to making ACFB a commercial technology option at utility scale. At 110

▼ Nucla Station, repowered with a circulating fluidized-bed boiler, was the world's first utility-scale AFBC unit in commercial service.

MWe, the Nucla ACFB unit was more than 40 percent larger than any other ACFB at that time. Up to 95 percent SO_2 removal was achieved during the 15,700 hours of demonstration and NO_x emissions averaged a very low 0.18 lb/10^6 Btu. The thrust of this effort was to fully evaluate the environmental, operational, and economic performance of ACFB. As a result, the most comprehensive database on ACFB technology available to date was developed. From this knowledge, commercial units were offered and built.

While the Nucla project established commercial acceptance of ACFB at moderate utility capacities, a second CCT demonstration project, located in Jacksonville, Florida, is carrying on where Nucla left off. JEA will build a 300 MWe plant, which will have the distinction of being the largest ACFB in the world, as well as one of the cleanest.

Today, every major U.S. boiler manufacturer offers an ACFB in its product line. There are now more than 170 fluidized-bed combustion boilers of varying capacities operating in the U.S. and the technology has made significant market penetration abroad.

Through the Ohio Power Company's repowering of the Tidd Plant (70 MWe), the potential of PFBC as a highly efficient, very low pollutant emission technology was established and the foundation was laid for commercialization. The PFBC system constructed was the first utility-scale system in the United States. Efforts were focused on fully evaluating the performance potential. Over 11,444 hours of operation, the technology successfully demonstrated SO_2 removal efficiencies up to 95 percent with very high sorbent utilization (calcium-to-sulfur molar ratio of 1.5) and NO_x emissions in the range of 0.15 to 0.33 lb/10^6 Btu.

The Tidd Plant PFBC was one of the first generation 70-MWe P200 units installed in the early 1990s. Others were built and operated in Sweden, Spain, and Japan. ABB Carbon, the technology supplier, uses a "bubbling" fluidized-bed design, which is characterized by low fluidization velocities and use of an in-bed heat exchanger. The first 360-MWe P800 PFBC is being built in Japan and is scheduled for operation in 1999. And, a "second generation" P200 PFBC, with freeboard-firing is under construction in Cottbus, Germany. A number of other ABB Carbon PFBC projects are under consideration in China, South Korea, the United Kingdom, Italy and Israel.

Two ongoing interrelated projects, McIntosh 4A and McIntosh 4B, will demonstrate pressurized circulating fluidized-bed technology (PCFB) at utility scale. PCFB uses a higher fluidization velocity than bubbling-bed systems, which entrains the bed material. Bed material is separated from the flue gas by cyclones and recirculated to the combustor. The economizer, which captures heat from the flue gas, is downstream of the cyclones. McIntosh 4A will evaluate a 145-MWe first generation PCFB configuration using Foster Wheeler technology. McIntosh 4B will demonstrate a second generation system by integrating a small coal gasifier (pyrolyzer) to fuel the gas turbine "topping cycle" (adding 93 MWe capacity). The second generation PCFB has the potential to significantly improve the efficiency of pressurized fluidized-bed systems by increasing power generation from the gas turbine, which is more efficient than the steam bottom cycle.

▼ Three IGCC plants are in various stages of operation: Tampa Electric (top), Piñon Pine (lower left), and Wabash River (lower right).

Integrated Gasification Combined Cycle. Three of four IGCC projects are in various stages of operation under the CCT Program. They represent a diversity of gasifier types, cleanup systems, and applications. PSI Energy's 262-MWe Wabash River Coal Gasification Repowering Project began operation in November 1995 and continues in its third year of commercial service. The utility dispatches the unit over other coal-fired units because of its high efficiency. The unit, which is the world's largest single train IGCC, has produced approximately 1.6 million megawatt hours of electricity on syngas through early 1998 and in March 1998 alone generated a record one trillion Btus of syngas.

The 250-MWe Tampa Electric Integrated Gasification Combined-Cycle Project began commercial operation in September 1996 and continues to accumulate run time. Availability steadily increased over time, reaching 70 percent for the past 12 months. The gasifier has accumulated over 10,000 hours of operation and produced over 2,000,000 MWh of electricity on syngas. Tests have included evaluation of various coal types on system performance.

The Sierra Pacific Power Company (SPPC) readies for sustained operation of its IGCC system on syngas. The 99-MWe Piñon Pine IGCC Project at SPPC's Tracy Station began operation on natural gas in November 1996. The GE Frame 6FA, the first of its kind in the world, performed well. The plant has undergone shakedown and design modifications have been made. The system routinely achieved steady state gasifier operation for short periods through September 1998.

The Clean Energy Demonstration Project, which is in the design stage, will offer yet another gasifier design and include the testing of a fuel cell operated on syngas from the coal gasifier. This will provide valuable data for design of an integrated gasification fuel cell (IGFC) system. IGFC has the potential to achieve efficiencies greater than 60 percent.

Commercial configurations resulting from the current IGCC and PFBC demonstrations will typically: have efficiencies at least 20 percent greater than conventional coal-fired systems (with like CO_2 emission reductions), remove 95 to 99 percent of the SO_2, reduce NO_x emissions to levels equivalent to a 90 percent reduction, reduce particulate emissions by 1/3 to 1/10 that currently allowed under the CAAA, and produce salable by-products from solid residues as opposed to waste.

Advanced Combustion/Heat Engines. Two projects are demonstrating advanced combustion/heat engine technology.

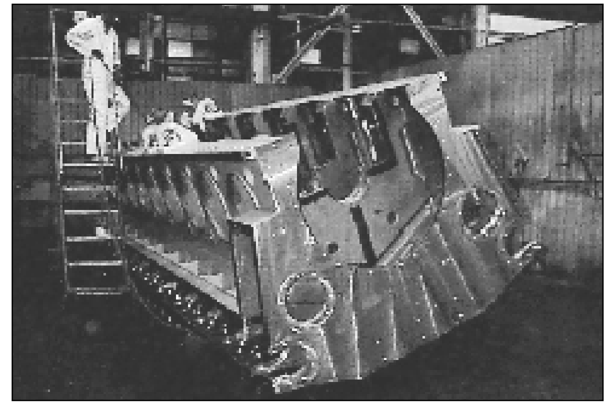
The Healy Clean Coal Project is demonstrating TRW's entrained (slagging) combustor combined with Babcock & Wilcox's spray-dryer absorber using sorbent recycle. Operations commenced in January 1998. Preliminary results have showed very low emissions—0.25 lb/10^6 Btu for NO_x and 0.08 lb/10^6 Btu for SO_2. Permit levels are 0.35 lb/10^6 Btu for NO_x and 0.10 lb/10^6 Btu for SO_2 because of the plant's proximity to a national park. NSPS allows 1.2 lb/10^6 Btu for SO_2.

The Clean Coal Diesel Demonstration Project is based on the demonstration of a heavy duty diesel engine to operate on a low-rank coal-water fuel. The demonstration plant is expected to achieve 41 percent efficiency and future commercial designs are expected to reach 48 percent efficiency. Operation is expected to begin in 1999.

Commercialization successes for the advanced electric power generation systems to date are summarized in Exhibit 4-4.

Coal Processing for Clean Fuels

Physical and chemical processes can be used on the abundant U.S. coal reserves to transform raw coal to an economic, environmental compliant fuel for at least a portion of the existing coal-fired boilers. The solid products from coal processing are easily transportable fuels; high in energy density; and low in sulfur, ash, and moisture. In addition, coal processing creates the capability to generate liquid fuels from coal that can replace petroleum and petroleum-based fuels in a wide range of applications, thereby enhancing the nation's energy security. The liquid products are suitable as transportation and stationary power generation fuels, or as chemical feedstocks. Both solid and liquid products, and the processes that produce them, have substantial market potential both domestically and internationally.



▲ Pielstick diesel engine block being cleaned prior to assembly in Beliot, Wisconsin.

The ENCOAL and Rosebud SynCoal Partnership projects are breaking down the barrier to using the nation's vast low-sulfur, but low-energy-density western coal resources. The resultant fuels have particular application domestically for CAAA compliance and internationally for Pacific Rim energy markets.

ENCOAL's solid fuel product has an energy density of about 11,000 Btu per pound and the sulfur content averages 0.36 percent. ENCOAL's liquid fuel product can substitute for No. 6 fuel oil or serve as a chemical feedstock. During the demonstration, over 83,500 tons of solid fuel was shipped to seven customers in six states, as well as 203 tank cars of liquid product to eight customers in seven states. Five commercial feasibility studies have been completed — two for Indonesia, one for Russia, and two for U.S. projects. Permitting of a 15,000 metric ton/day commercial plant in Wyoming is nearly complete.

The Rosebud SynCoal® project is demonstrating another route to producing high-quality fuel from low-rank coals. The advanced coal conversion process (ACCP) upgrades low-rank coal to produce a low-

Exhibit 4-4
Commercial Successes—Advanced Electric Power Generation

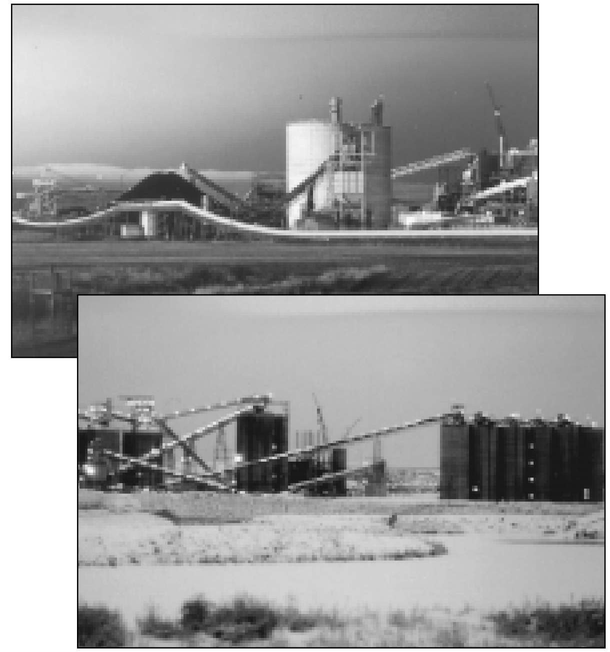
Project and Participant	Commercialization Progress
Tidd PFBC Demonstration Project (The Ohio Power Company)	First utility-scale PFBC in U.S. – Laid foundation for commercialization of PFBC The first 360-MWe ABB Carbon P800 PFBC plant is being built in Japan A second generation ABB Carbon P200 PFBC is under construction in Germany Other ABB Carbon PFBC projects are under consideration in China, South Korea, the United Kingdom, Italy, and Israel
Nucla CFB Demonstration Project (Tri-State Generation and Transmission Association, Inc.)	Technology retained for commercial use at host site – World's first large utility-scale ACFB Demonstration commercialized utility-scale ACFB – Quantity—29 CFB units larger than 100 MWe planned, in construction, or in operation worldwide – Estimated capacity—greater than 6,200 MWe – Estimated value—almost $6 billion
Tampa Electric Integrated Gasification Combined-Cycle Project (Tampa Electric Company)	First greenfield IGCC unit in commercial service Texaco, Inc., and ASEA Brown Boveri signed an agreement forming an alliance to market IGCC technology in Europe
Wabash River Coal Gasification Repowering Project (Wabash River Coal Gasification Repowering Project Joint Venture)	First repowered IGCC unit in commercial service – World's largest single train IGCC in commercial service – Preferentially dispatched over other coal-fired units in PSI Energy's system because of high efficiency
Piñon Pine IGCC Power Project (Sierra Pacific Power Company)	Unit in initial operation preparatory to commercial service
Healy Clean Coal Project (Alaska Industrial Development and Export Authority)	TRW offering licensing of combustor worldwide (China agreement in place)

sulfur (as low as 0.3 percent sulfur) SynCoal® product having a heating value of about 12,000 Btu per pound. By the end of September 1998, more than 1.4 million tons of SynCoal® had been produced. Nearly 1.3 million tons has been supplied to industrial applications and utilities. The Rosebud SynCoal® Partnership has signed a letter of agreement to supply fuel to Montana Power's 330-MWe Colstrip Unit No. 2.

Advanced physical coal-cleaning technology developed by Custom Coals International uses high-sulfur bituminous feedstocks to produce two types of compliance coal—Carefree Coal™ and Self-Scrubbing Coal™.

Air Products Liquid Phase Conversion Company, L.P., is demonstrating the LPMEOH™ process to produce methanol from coal-derived synthesis gas.

▼ Coal processing technologies remove barriers to the use of low-energy-density western coal resources: Rosebud (top) and ENCOAL (bottom).



The LPMEOH™ process has been developed to enhance integrated gasification combined-cycle power generation facilities by coproducing a clean-burning storable liquid fuel from coal-derived synthesis gas. The production of dimethyl ether (DME) as a mixed coproduct with methanol will also be demonstrated. Methanol and DME may be used as a low-SO_2, low-NO_x alternative liquid fuel, a feedstock for the synthesis of chemicals, or as a new oxygenate fuel additive.

The first stable operation of the LPMEOH™ unit at nameplate capacity of 80,000 gallons per day was achieved in April 1997, only four days after start-up. A test period at methanol production rates over 92,000 gallons per day has demonstrated the potential for this new technology.

Exhibit 4-5
Commercial Successes—Coal Processing for Clean Fuels

Project and Participant	Commercialization Progress
Development of the Coal Quality Expert™ (ABB Combustion Engineering, Inc., and CQ Inc.)	CQ Inc. and Black & Veatch working collaboratively to commercialize CQE™ worldwide CQE's Acid Rain Advisor licensed to two U.S. users 30 U.S. and 1 U.K. utilities acquired CQE™ through EPRI membership Other foreign and domestic utilities pursuing access to CQE™ CQE technology saves U.S. utilities $26 million CQE™ Home Page posted on World Wide Web (http://www.fuels.bv.com:80/cqe/cqe.htm)
Self-Scrubbing Coal™: An Integrated Approach to Clean Air (Custom Coals International)	Proposed agreement to purchase 1 million tons/yr in U.S. Proposed agreement with China to build a coal-cleaning plant, slurry pipeline, and port facility – Value—$450 million Letter of intent for three additional pipelines in China – Value—$3 billion Letters of intent from Polish utilities for 5 million tons/yr – Value—$50 million
Advanced Coal Conversion Process Demonstration (Rosebud SynCoal Partnership)	Total sales of SynCoal® product exceeds 1,400,000 tons A commercial project being developed – Stand-alone minemouth design in Wyoming
ENCOAL® Mild Gasification Project (ENCOAL Corporation)	Over 83,500 tons of solid fuel delivered to seven major utilities and metallurgical customers Over 200 tank cars of liquid fuel delivered to eight industrial users Permitting of a 15,000 metric-ton/day commercial plant in Wyoming is nearly complete – Value—$460 million Completed five feasibility studies—two Indonesian, one Russian, and two U.S. projects
Commercial-Scale Demonstration of the Liquid Phase Methanol (LPMEOH™) Process (Air Products Liquid Phase Conversion Company , L.P.)	Nominal 80,000 gallon/day methanol production being used by Eastman Chemical Company

Since start-up, the LPMEOH™ demonstration unit has produced over 25 million gallons of methanol, all of which was accepted by Eastman for use in downstream chemical processing. Since restart of the unit with fresh catalyst in December 1997, availability of the unit has been greater than 99 percent and catalyst activity decline has been less than 0.4 percent.

ABB Combustion Engineering, Inc., and CQ Inc. developed PC-based software, CQE™, to assist utilities in assessing the environmental and operational performance of their systems for the available range of coal fuels to determine the least-cost option. The CQE™ software has been distributed to over 30 utility members of EPRI and is being marketed commercially worldwide. Two U.S. utilities also have been licensed to use copies of the CQE™ stand-alone Acid Rain Advisor.

Commercialization successes for the coal processing technologies to date are summarized in Exhibit 4-5.

▼ The LPMEOH™ demonstration unit at Eastman's vast chemicals-from-coal complex in Kingsport, TN.

Industrial Applications

The CCT Program is addressing the environmental issues and barriers associated with coal use in industrial applications. Historically, production of steel has been dependent upon coke. Coke making, however, is an inherently large producer of SO_2, NO_x, and hazardous air pollutants. Also, cement production often relies on coal fuel because production costs are largely driven by fuel costs. Because of its low stable price, coal is an attractive substitute for oil and gas in industrial boilers, but concerns over increased SO_2 and NO_x emissions and boiler tube fouling have impeded coal use.

Under a project with Bethlehem Steel Corporation, British Steel's blast furnace granular-coal injection technology demonstrated that 40 percent of the coke can be replaced with coal injected directly into a blast furnace where emissions from coal combustion are effectively controlled in the process.

CPICOR™ is in the design stage of demonstrating a direct iron ore reduction and smelting of iron oxides using coal in lieu of coke. This would eliminate the need for coke.

The Passamaquoddy Tribe successfully demonstrated a unique recovery scrubber that uses cement kiln dust, otherwise disposed of as waste, to remove 90 percent of the SO_2, produce fertilizer and distilled water, and convert the kiln dust to feedstock with no waste generated.

Coal Tech Corporation moved closer to commercializing a combustor for industrial boilers that slags the ash in the combustor to prevent boiler tube fouling, controls NO_x (70 to 80 percent reduction) through staged combustion, and controls SO_2 (90 percent) with sorbent injection.

Exhibit 4-6
Commercial Successes—Industrial Applications

Project and Participant	Commercialization Progress
Blast Furnace Granular-Coal Injection System Demonstration Project (Bethlehem Steel Corporation)	British Steel granted exclusive marketing rights to technology co-developer, CPC-Macawber Commercial sale of technology to United States Steel Corporation
Cement Kiln Flue Gas Recovery Scrubber (Passamaquoddy Tribe)	Technology retained for commercial use at host site Completed feasibility study for Taiwanese cement plant

ThermoChem, Inc. has completed restructuring of its project and will be demonstrating a multiple resonance tube pulse combustor design.

Commercialization successes for the industrial applications technologies to date are summarized in Exhibit 4-6.

Market Communications–Outreach

Outreach has been a hallmark of the CCT Program since its inception. It was recognized early on that commercialization of technology requires acceptance by a range of interests including: technology users; equipment manufactures; suppliers and users of raw materials and products; financial institutions and insurance underwriters; government policy makers, legislators, and regulators; and public interest groups. Requisite to acceptance is an outreach program to provide these customers and stakeholders with both program and project information and to seek, on a continuing basis, feedback on program direction and information requirements. An ongoing outreach program has aggressively sought to disseminate key information to the full range of customers and stakeholders and to obtain feedback on changing needs. The effort has recognized the need to highlight environmental, operational, and economic performance characteristics of clean coal technologies and to redesign information packages as customers and stakeholders, and their respective needs, change with the market. Specific objectives of the outreach program include the following:

- Achieving public and government awareness of advanced coal-using technologies as viable energy options;
- Providing potential technology users, both foreign and domestic, with information that is timely and relevant to their decision making process;
- Providing policy makers, legislators, and regulators with information about the advantages of clean coal technologies;
- Increasing the confidence of financial institutions and insurance underwriters that clean coal technologies are viable options; and

Exhibit 4-7
How to Obtain Updated CCT Program Information

Media	Description and Action
Clean Coal Today	Subscription to quarterly newsletter—Send name and address to U.S. Department of Energy, FE-24, Washington, DC 20585.
Fossil Energy TechLine	Fax-on-demand system for news announcements and status reports—Call (202) 586-4300 from a tone phone and follow voice instructions or call (202) 586-6503 for additional TechLine information.
Computer Bulletin Board	Dial (202) 586-6495 via modem.
Fossil Energy Home Page	Primary gateway to extensive information on DOE's Fossil Energy Program and to relevant Web links—On the Internet, access http://www.fe.doe.gov and use menu and/or search options.
CCT Compendium	On the Internet, access http://www.lanl.gov/projects/cctc/.
CCT Program Update and other publications	Send name and address to U.S. Department of Energy, FE-20, Washington, DC 20585.
National Technical Information Service (NTIS)	U.S. Department of Commerce, 5285 Port Royal Road, Springfield, VA 22161 (703-487-4600).

- Providing forums and opportunities for feedback on program direction and information requirements.

Information Sources

A portfolio of publications and information access media exist and are being improved upon as program and marketplace events unfold. Information is currently distributed to over 4,000 customers and stakeholders, 275 of which are CCT project participants. The following provides a brief synopsis of the publications and information transfer mechanisms currently in place or soon to be introduced:

Clean Coal Technology Demonstration Program: Annual Program Update provides an annual summary of program and project progress, accomplishments, and financial status along with an historical backdrop and program role relative to current policy.

Annual Clean Coal Technology Conference Proceedings serves as an annual update on issues impacting the program, feedback on program direction, and a yearly snapshot of how each of the active projects is progressing with some degree of technical depth.

Clean Coal Technology Demonstration Program: Project Fact Sheets provides a mid-year update on each project.

Clean Coal Today Newsletter offers the readership a quarterly look at the program, highlighting key events, updating project status, and listing the latest publications and upcoming events.

Topical Reports capture projects at critical junctures and highlight particular technological advantages, project plans, and expected outcomes.

National Technical Information Service (NTIS) serves as the Federal government's central source for the sale of scientific, technical, engineering, and related business information produced by or for the U.S. government. NTIS has most of CCT Program technical reports.

CCT Program Bibliography of Publications, Papers, and Presentations periodically updates the key materials available on the technologies demonstrated under the CCT Program.

The Investment Pays Off periodically takes a market-based view of the success of the CCT Program by virtue of commercial sales and relevance of ongoing activities to projected market need.

CCT Program - Lessons Learned documents the lessons learned in soliciting, selecting, and awarding projects and implementing the program.

CCT Compendium provides an electronic database incorporating the CCT Program publications that can be accessed on the Internet (http://www.lanl.gov/projects/cctc/).

Exhibits provide a means through graphics, photos, broadcast videos, and interactive videos to convey program messages at a variety of forums and serve as focal points for distribution of literature and discussion of the program and information needs. (There are currently four exhibits of varying sizes and complexity that are updated and modified, as necessary, to convey the appropriate message for specific forums.)

Fossil Energy Techline offers fax-on-demand for news announcements and status reports on projects (202-586-6503).

Computer Bulletin Board offers a modem accessed bulletin board of noteworthy items on the CCT Program (202-586-6495).

Fossil Energy Home Page provides the primary Internet gateway to extensive information on DOE's Fossil Energy Program and to relevant World Wide Web links (http://www.fe.doe.gov).

Exhibit 4-7 summarizes how the above publications can be obtained and information sources can be accessed.

Publications Issued in FY1998

The following publications were issued in Fiscal Year 1998 by the CCT Program. Similar publications can be expected in Fiscal Year 1999.

CCT Program Bibliography of Publications, Papers, and Presentations

Sixth Annual Clean Coal Technology Conference: What Will It Take?; Technical Papers

Sixth Annual Clean Coal Technology Conference: What Will It Take?; Proceedings

Clean Coal Technology Demonstration Program: Program Update 1996-97

Clean Coal Technology Demonstration Program: Project Fact Sheets 1997

Clean Coal Today: Winter 1997, Spring 1998, Summer 1998, Fall 1998

Clean Coal Today Index

Information Access Updates for FY1998

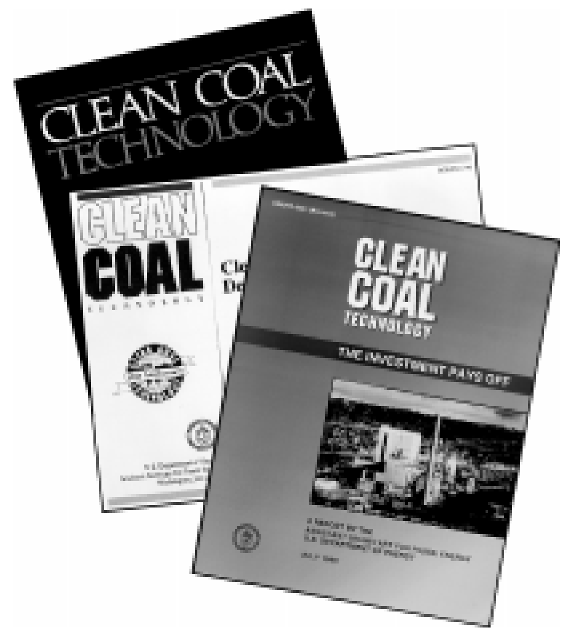
The Department of Energy continued to expand its website, accessible through the Internet that provides information on federal fossil energy programs and serves as a "gateway" to other related information throughout the United States and the world. Once into the DOE website, users can obtain general information and follow links to increasingly detailed information, ultimately accessing specific data on individual projects and facilities. Hyperlinks allow users to move seamlessly between headquarters and field sites. Users can also access technical abstracts and reports maintained by DOE's Office of Scientific and Technical Information at Oak Ridge, Tennessee. The gateways link to more than a hundred energy-related websites operated by private companies, trade associations, and other agencies worldwide.

▼ One of four clean coal technology exhibits, shown here, was used at the Sixth Annual CCT conference to convey a technical message.

Furthermore, the Fossil Energy International Activities site on the World Wide Web has been expanded with the addition of new country pages in the Western Hemisphere region (Guatemala, Honduras, Nicaragua, Paraguay, Trinidad & Tobago, and Uruguay) and the Russia/NIS region (Armenia, Georgia, and Moldova). Many of the existing country pages have also been upgraded, with new hyperlinks to business- or energy-related information sources. An innovation at the Fossil Energy International Activities web site is a series of newly created Country Energy Overviews. Each overview, individualized for a particular country, includes a status summary of that country's energy infrastructure, energy and environmental policies, and privatization efforts. Seven country pages in the Eastern Europe region now include these overviews; Western Hemisphere country pages will be next to receive these upgrades. The Uniform Resource Locator (URL) for the Fossil Energy International main page is http://www.fe.doe.gov/international and can be accessed via the "International" hyperlink in the Fossil Energy Home Page (http://www.fe.doe.gov).

In February 1998, DOE established a new information resource on the Internet. The Clean Coal Technology Compendium, sponsored by the Office of Fossil Energy and the Federal Energy Technology

▼ The CCT Program reports progress and accomplishments through several publications distributed to almost 4,000 customers and stakeholders.



Center (FETC), is dedicated to making the maximum use of information derived from the CCT Program. The compendium designers anticipate that the compendium will become the principal source of information for stakeholders interested in implementation of clean coal technologies. The compendium is designed to emphasize ease of use, and contains a broad collection of different types of data and information, making it applicable to the needs of both managers and engineers. For example, by selecting the CCT Program menu option, one can access the latest CCT Demonstration Program Annual Program Update, and Topical Reports published periodically on individual CCT projects. The Compendium is accessible via the Internet at http://www.lanl.gov/projects/cctc/.

Information Dissemination and Feedback

A number of mechanisms are used to disseminate program information to customers and stakeholders and obtain feedback from them on specific issues, program direction, and information requirements. The following provides a brief outline of the mechanisms.

Public Meetings were routinely held over the course of the acquisition phase of the CCT Program to solicit input on procurement actions. Subsequently, project participants have been holding open houses for the public, providing tours of demonstration facilities, and publicizing projects through groundbreaking and dedication ceremonies.

Executive Seminars involve program officials meeting with key industry officials at their places of business to facilitate discussion. Discussions seek to: obtain a better understanding of the dynamics of the decision making process for adopting new power generating technologies, determine how the program could best support the process and achieve a positive outcome, and gain insights on the future direction of the power industry. Over 50 meetings have been held since 1992 with influential leaders in the utility, independent power, regulatory, and financial communities.

▲ The CCT Program exhibit serves as a focal point for distribution of literature and discussion of the program.

Stakeholder Meetings bring together key stakeholder organizations for the purpose of coordinating programs, where appropriate, and discussing pertinent issues and implementation strategies to address the issues, and outreach needs. Such stakeholder organizations include the Electric Power Research Institute (EPRI), Gas Research Institute (GRI), Coal Utilization Research Council, Center for Energy & Economic Development (CEED), Council of Industrial Boiler Owners (CIBO), Clean Coal Technology Coalition, and National Mining Association (NMA).

Conferences and Workshops bring together targeted audiences to review and discuss topics of interest, document discussions and findings, and provide recommendations, as appropriate. *Trade Missions* are a subset of these and differ only in that the thrust is international in character with the purpose of promoting the export of U.S. services and technology. The outreach program has participated in over 200 technical conferences, workshops, and trade missions since 1991.

Sixth Annual Clean Coal Technology Conference: What Will It Take?

Some 340 attendees from 22 countries participated in the Sixth Annual Clean Coal Technology Conference held in Reno, Nevada from April 28 to May 1, 1998. Cosponsors included the CEED, NMA, EPRI, CIBO, and DOE. Sierra Pacific Power Company hosted the conference and a site visit to its Tracy Station which employs IGCC technology.

The Conference provided an annual update on the CCT Program, the issues driving technology decisions, and suggested courses of action to affect technology deployment.

The Department of Energy Assistant Secretary for Fossil Energy set the stage for the Conference by recognizing CCT Program accomplishments and challenging participants to define what it will take to finish the job—deploy CCTs on a large scale into U.S. and global energy markets. Participants were encouraged to find ways: to leverage the investment in CCTs and the attendant databases; to work with international organizations toward increased use of CCTs in near-term overseas markets; and to develop innovative incentives and financial mechanisms for CCTs, aside from subsidies.

The Assistant Secretary also outlined DOE's efforts to build on the CCT experience toward achieving "Vision 21," where power-plexes would squeeze every available Btu out of coal, and produce multiple products in lieu of pollutant emissions and waste. But it was recognized that Vision 21 efficiency improvements alone may not be enough, which has prompted exploration of CO_2 sequestration options.

Domestic Market. Panel discussions identified two basic issues that currently drive technology decisions in the domestic market—environmental concerns and utility restructuring. Discussion of environmental concerns focused on the most significant challenges. Utility restructuring discussions addressed potential implications for power generators. The following highlights some of the findings.

Environmental Concerns. The CCT Program has provided a portfolio of technologies to effectively deal with acid rain concerns. Challenges remain, however, in achieving ozone standards (a NO_x control issue), fine particulate control ($PM_{2.5}$), and CO_2 emission reduction.

Ozone nonattainment prompted the EPA to issue a NO_x transport SIP Call for 22 states to meet the following:

Date	NO_x Emissions
May 1999	0.2 lb/10^6 Btu
2003	1.5 lb/10^6 Btu
2007	Cap emissions

Utilities have expressed concern that the proposed compliance schedule does not allow sufficient time to develop a cost effective response. Selective Catalytic Reduction represents the only option currently available, and little experience exists with U.S. high-sulfur coals. Capping NO_x emissions in 2007 may push technology beyond the capability of SCR.

Evaluation of $PM_{2.5}$ fine particulate emissions may lead to a requirement for additional SO_2 reductions associated with sulfate formation from stack gases. However, even complete particulate emission control cannot prevent compounds precipitated from post-stack chemical reactions.

CO_2 reduction per the Kyoto Protocol may spell disaster for coal-based power generation in the absence of trading between developed and developing countries under a proposed Clean Development Mechanism (CDM) and/or sequestration.

Utility Restructuring. Utility restructuring is moving rapidly forward with some 40 percent of the states sponsoring conceptually and functionally different legislation. Some argue that federal legislation is needed to provide some consistency in what they consider will be a “crazy quilt” of implementing mechanisms. State legislation is driven by different rate structures, fuel mixes, stranded cost implications, and environmental policies. Federal legislation is being deliberated.

The electric power industry embraces the concept of open competition, but some speakers expressed concern that legislation is skewing the market away from market-based outcomes by establishing “Renewable Portfolio Standards,” which would require sellers to include an increasing proportion of above-market cost renewable generation in their annual sales over time.

Competition will spur generators to increase capacity factors on existing plants to meet increased demand and also upgrade existing plants where there is significant potential to increase both efficiency and capacity. Existing coal-fired plant upgrades might lead to efficiency improvements of 2 to 4 percent and capacity increases of 10 to 13 percent.

Restructuring has the potential to remove barriers to distributed power systems. Distributed power can produce significant efficiency improvements relative to central power generation because there are no line losses and heat, steam, and other byproducts can be readily utilized.

Competition will drive a paradigm shift for power generators to a commodity viewpoint with the commodities being electricity, heat, steam, and chemical byproducts. Providing a multiplicity of commodities enhances market potential and reduces risk.

In a market-based utility industry, coal-based technologies must meet the challenge of $800/kW capital cost (at acceptable risk) while complying with all environmental standards and without guarantee of cost recovery. The Coal Utilization Research Council shows 30-year levelized cost of electricity for advanced coal-based systems (7,000 Btu/kWh heat rate) to be competitive with natural gas-fired systems by 2020 at $800/kW, and year 2000 coal and gas prices of $1.30/$10^6$ Btu and $2.25/$10^6$ Btu respectively. To achieve $800/kW, more CCTs must be installed and designs refined to mitigate risk and cost. The importance is underscored by the fact that financing will be more difficult in a deregulated environment, where customers are no longer required to cover capital investments in the rate base.

Employing IGCC to co-produce power and syngas-derived products may provide an avenue for this technology to enter the marketplace. The key initially is to find low-cost disadvantaged fuels such as heavy petroleum liquids or petroleum coke. For some applications, syngas conversion alone may be the best option. These applications will serve to reduce the risk and cost of IGCC technology. There is some movement domestically toward installing gasification-based systems for co-production.

International Market. An International Business Forum was held at the conference to identify emerging opportunities for CCTs worldwide. The following presents some of the key points made during the forum.

Market Definition. While the near-term domestic market for CCTs is not promising, the international market for CCTs has tremendous near-term potential. Basic elements exist in many developing countries for CCTs to play a major role in meeting energy demands. For many, coal is the primary indigenous fuel, and the need for jobs and mitigation of poverty may reduce the stigma global climate change associates with coal.

The total world power market between now and 2010 is estimated to be 950 GW. Of that total 50 percent resides in Asia, 30 percent in Europe, and 20 percent in the Americas. Within Asia, China alone has 16 percent of the total market, Japan/Indonesia/Korea have 17 percent, and India alone has 6 percent. These numbers, plus reliance on coal in the Asian market, make it the primary target for CCTs.

Realizing Market Potential. Realizing market potential for CCTs requires action to mitigate the higher risk and cost of CCTs. Environmentally superior performance of CCTs serves as an incentive, but costs must be competitive with other options. Cost saving measures can be taken, such as using disadvantaged fuels, producing multiple commodities, and firmly defining projects to reduce contingencies. Trading mechanisms for CO_2, such as the 161-nation "Global Environmental Facility" and others proposed under the Kyoto Protocol, hold promise for obtaining incremental cost decreases for CCTs, assuming CO_2 reduction requirements or incentives are formalized.

▼ An interactive exhibit at the Sixth Annual Clean Coal Technology Conference.

Fluidized-bed combustion technology, the most mature CCT power system technology, has made inroads into foreign markets because of its tremendous fuel flexibility and proven track record. This demonstrates the possibilities for the more advanced systems. IGCC is already making progress through use of disadvantaged fuels and production of multiple commodities. There are some 20 known IGCC projects worldwide, 10 already in place, and 10 more in the planning stage.

Conferences and Workshops Held in FY1998

Fifth Annual Technical Seminar of Asia-Pacific Economic Cooperation (APEC) Expert's Group on Clean Fossil Energy. The Office of Fossil Energy participated in the APEC technical seminar. This seminar, held in Reno, Nevada, in October 1997, brought together senior energy policy officials from around the globe. It followed a series of four previous meetings of the Expert's Group held in Thailand, Indonesia, South Korea, and the People's Republic of China.

Historically, APEC nations have been able to gain insight into the plans and actions of all member countries while at the same time being afforded an opportunity to participate in the formulation of policies, procedures, trade regulations, and other issues that impact individual economies. Of interest to members are environmental and economic factors and functions. In particular, APEC has provided a forum for encouraging coal use in the Pacific Rim, and has expended a great deal of effort to make coal a high-profile fuel. Australia and the United States share the lead responsibility for the energy and environment activity, which emphasizes coal and clean coal technology. The goal of this activity is to assist APEC members in reducing their dependency on imported oil by using more coal, increasing efficiency of energy use in the region, and promoting U.S. energy exports.

Executive Committee Meeting of the IEA Clean Coal Center. In October 1997, representatives from the Office of Fossil Energy participated in the Executive Committee meeting of the International Energy Agency's (IEA) Clean Coal Center, the International Energy Agency's coal research activity. The Committee agreed to initiate studies in the following areas: blast furnace coal injection; management of coal stockpiles; opportunities for coal preparation to lower emissions; particulate emissions from coal combustion (PM_{10}, $PM_{2.5}$); computers and air pollution control; a NO_x control systems database; coal-fired power stations and water quality; and coal-fired power generation and air pollution control in South Asia.

International Symposium on Clean Coal Technology. A team from the Office of Fossil Energy participated in the symposium, co-sponsored by DOE, China's Ministry of Coal Industry (MOCI), and the European Commission Directorate of Energy. The conference took place in Xiamen, Fuijan, China, on November 17-21, 1997. In parallel with the conference was a workshop sponsored by the Fuijan Coal

Industry Administration of MOCI, a group heavily involved in a variety of coal-related projects. The workshop was targeted toward specific clean coal projects and opportunities in Fuijan.

Ukraine/U.S. Joint Conference on Ukraine Clean Coal Power Plant Upgrade Opportunities. On April 21-22 , 1998, some 160 attendees (30 from the U.S.) participated in the conference held in Kiev. The conference was co-sponsored by U.S. DOE, U.S. Agency for International Development, and the Ukrainian Ministry of Energy and Electrification. The conference was held to report on the recently finished study on upgrading the anthracite-fired Lugansk Power Station in eastern Ukraine with the goal of obtaining World Bank financing, and to provide a forum for exchange of information among Ukrainian government and power sector officials and western companies interested in rebuilding that country's aging coal-fired power sector.

Advanced Coal-Based Power and Environmental Systems '98 Conference. The Department of Energy hosted the July 21-23, 1998, conference in Morgantown, West Virginia. About 300 persons attended the conference representing every region of the United States and several other countries.

The conference provided a forum for industry representatives, government regulators, scientists, engineers, and other interested parties to: (1) share the results of FE-sponsored research and development projects related to advanced power generation and environmental systems; (2) learn about cooperative industrial-government research and development opportunities (CRADAs) with FETC; and (3) discuss the direction of future research and development for a competitive energy market in the coming millennium.

Industrial and academic researchers and developers, along with FETC scientists and engineers, presented research results at sessions for Advanced Power Systems; IGCC Gas Cleaning, Recovery, Separation, and Advanced Gasification; Particulate Control; By-Product Utilization; Environment Control Technology; and Global Climate Change. Two poster sessions were also held for Combustion and Environmental Control, and Hot Gas Cleanup.

Trade Mission Activities in FY1998

Brazil. Following over a years's effort, during which the Office of Fossil Energy provided significant guidance, support, and advice, the U.S. Trade Development Agency (TDA) announced a grant of $470,000 for a feasibility study for a new coal-fired power plant in Brazil. The grant will be awarded to Copelmi Mineracao, S.A., one of Brazil's largest coal producers. The new coal-fired power plant is to be located near the Seival coal mine in Rio Grande do Sul. The area is Brazil's third most populous and industrialized state, and is experiencing rapid industrial growth. Average energy consumption for the state is at approximately 3,000 MWe while it only produces 700 MWe. Total cost of the new mine-mouth plant is estimated at $400 million. When the project is finally approved, engineering, new generation equipment, instrumentation, controls, construction, and management services will all be open for bidding to U.S. firms. TDA also recently approved another grant in the amount of $140,000, cost-shared with mine owner Copelmi Mineracao, to study Seival coal mine development options.

During FY1998, U.S. DOE's Office of Import and Export and the Southern States Energy Board co-sponsored a Conference in Atlanta, Georgia to promote the many business opportunities involved in the multi-million dollar projects planned in Brazil.

▲ Governor of West Virginia and Brazilian industrialists confer on coal investment opportunities at Atlanta conference.

China. The 14th International Pittsburgh Coal Conference, held in Taiyuan, China September 23-25, 1997, was attended by over 300 delegates representing 18 countries and over 200 major international corporations, government agencies, research organizations, and educational institutions. In addition to the University of Pittsburgh, co-sponsors of the event included the Shanxi Energy Research Society (China), the Institute of Coal Chemistry, Chinese Academy of Sciences (China), and the U.S. DOE Federal Energy Technology Center (FETC). One of the highlights of the conference was the International Coal Forum. Distinguished panelists included key industrial leaders and policy makers from Babcock & Wilcox Power Generation Group, the Chinese National Power Corporation, the East-West Center, Hawaii, and the Atmospheric Environment Institute, China. Presentations emphasized the collaborative spirit in which the conference was organized, and set the tone for the exchange of technical information between the international and Chinese participants.

▲ FETC Director moderates International Coal Forum at the 14th International Pittsburgh Coal Conference in Taiyuen, China.

A major feature of the 14th International Pittsburgh Coal Conference Agenda was the U.S. sponsored two-day Clean Coal Technology and Coal Utilization Workshop, held on September 26-27, 1997, in Taiyuan, China. The workshop focused on economics and commercialization of demonstrated innovative and conventional technologies potentially applicable to markets in China and the Pacific Rim countries.

More than 120 technologists from China, the U.S., and sixteen other countries attended the workshop. Over 40 presentations were made by various representatives of the U.S. and Chinese industrial firms, with each presentation delivered to an audience of 25 to 50 attendees from the international community. Some 24 of the presentations represented U.S. clean coal technologies and coal utilization technologies. The remainder of the presentations represented Chinese use of clean coal and utilization technologies, and China's potential need for more and better applications. The format of the workshop encouraged discussions and the exchange of information.

On November 15, 1997, the Tsinghua University in Beijing, China held a commencement ceremony of the U.S.-China Energy and Environmental Technology Center (EETC). The EETC represents a significant step for the two countries in demonstrating a long-term relationship that builds on trust, mutual benefits, and good will.

EETC was created and made possible under joint DOE and EPA funding. Its mission is to enhance the competitiveness and adoption of U.S. clean and environmentally superior technologies in China by focusing on education and training, promoting the use and profitability of U.S. technology, and supporting policy development in China to encourage the responsible use of coal. The EETC activities are jointly implemented by the U.S. and the Chinese governments: U.S. DOE and EPA, China's State Science and Technology Commission (SSTC), Tulane University in New Orleans, and Tsinghua University. The Chinese government is cost-sharing part of EETC's activities. A bi-national core team composed of members from a number of U.S. and Chinese organizations is overseeing and implementing EETC's work.

Although the opening ceremony was held in November 1997, an EETC office has been operational at the Tsinghua University for nearly a year. The following are some of its accomplishments.

- Establishment of a web site and home page at http://www.tulane.edu/~uschina to support an Internet-based energy and environmental information system. The site includes a database of more than 1,000 U.S. firms with energy and environmental technology and equipment that can serve the Chinese market.
- The conduct of joint expert studies on coal liquefaction, IGCC for retrofit and repowering, coal preparation, and superfine coal applications, with plans to investigate applications for molten carbonate fuels cells. Studies include analysis of technology readiness, need for the technology in China, and barriers to technology introduction. Some assessments are generic while others are site-specific.
- Development of a model cogeneration contract for joint venture projects.

Korea. The Office Fossil Energy and the U.S. Department of Commerce co-sponsored the highly successful 12th Korea-U.S. Joint Workshop on Energy and Environment, in Taejon, Korea October 6-11, 1997. This year's workshop was combined with a trade mission so that the U.S. delegation included 36 representatives from 16 firms specializing in advanced power generation, air pollution control, and waste management, who met with potential Korean partners at on-the-spot appointments. On the Korean side, the workshop was organized by the Korea Institute of Energy Research and sponsored by the Ministry of Trade, Industry and Energy, with participation by the Korea Electric Power Corporation. Also participating were 124 Korean industry representatives. The workshop, which included a 2-day technical conference and site visits, achieved its major goal of introducing a broad range of U.S. energy and environmental companies to Korea and provided an effective forum for information exchange on energy and environmental technologies, for which there is a large Korean market.

Uruguay. The Office of Fossil Energy's Office of Coal and Power Systems sponsored the "Roundtable on the Deployment of Clean Power Systems for Power Generation Technologies" at the September 1997 "Meeting on Natural Gas and Electric Power Integration in the Southern Cone" held in Uruguay. The Government of Uruguay was overall conference host, and co-sponsored the workshop with the DOE, the Department of State, the Department of Commerce, and the U.S. Trade and Development Agency. Over 200 government officials and industry executives from the U.S., Argentina, Bolivia, Brazil, Chile, Paraguay, and Uruguay attended. The Roundtable consisted of sessions on Alternative Advanced Clean Energy Technologies, and Financing of Clean Energy Projects. U.S. representatives made presentations on IGCC, FBC, and fuel cells. Participants discussed potential areas of collaboration, opportunities for U.S. companies in Latin America, and barriers to business opportunities.

Japan. Office of Fossil Energy representatives participated in the 10th Annual FETC/Japanese Technical Meeting on Coal Liquefaction and Materials for Coal Liquefaction, held in Tokyo in October. The meeting provided an excellent opportunity for exchange of technical information. Participants also had the opportunity to tour Japan's 150 ton/day direct coal liquefaction demonstration plant outside of Tokyo. The demonstration plant, which went on-line in November 1996, is the largest in existence and will operate for three years to obtain scale-up data for a commercial plant and to evaluate the economic feasibility of the project.

Philippines. The Office of Fossil Energy sent a representative to the Philippines in the summer of 1998 to discuss potential application of clean coal technologies to the Palawan Province, an environmentally pristine area where all generation is currently oil-fired and 70 percent of the near-one million population live in isolated communities without power. Meetings have been conducted under the auspices of the Philippine Center for Sustainable Development, which was funded by the U.S.-Asian Environmental Partnership (a U.S. State Department program). The Center is a collaborative international institute started in 1997 by a California-based consortium led by California State University in Hayward and the Philippines' De La Salle University in Manila. The initial effort in Palawan, largely supported by local funding, will be a pilot program of modeling on and economic analysis of the role of advanced clean technologies, including clean coal, in the energy mix.

The Center's team comprises representatives from the Office of Fossil Energy, De La Salle University, California State University, Lawrence Livermore National Laboratory, and the University of California at Santa Barbara and at Davis. If the Palawan effort is successful, a national model would be developed with the Philippines' Ministry of Energy for other rural communities. Funding for that effort would be expected to come from a variety of international and local sources. The model also may be applicable to other

▲ Unveiling of a plaque at the dedication of the EETC.

Asian countries that are seeking a mix of energy generation to cope with growing economic demand while addressing climate change concerns.

Some 20 percent of Philippine power generation is coal-fired, with the remainder oil-fired. Oil is expected to be phased out, with new generation coming from natural gas and a combination of clean coal and renewables.

Switzerland. DOE co-sponsored the Fourth International Conference on Greenhouse Gas Control Technologies in Interlaken, Switzerland August 30–September 1998. The conference provided a forum for the discussion of the latest advances in the field of greenhouse gas control technologies, including capture, storage, and utilization. Also addressed were other mitigation options such as efficiency increase and use of renewables, as well as economic issues. An underlying objective of the conference was to promote international research and development collaborations and to encourage an exchange of ideas on future directions in this field. DOE participated by outlining its Vision 21 program and attendant carbon sequestration efforts, using an exhibit and handouts to underscore the message.

5. CCT Projects

Introduction

CCT Program demonstrations provide a portfolio of technologies that will enable coal to continue to provide low-cost, secure energy vital to the nation's economy while satisfying energy and environmental goals well into the 21st century. This is being carried out by addressing four basic market sectors: (1) environmental control devices for existing and new power plants, (2) advanced electric power generation for repowering existing facilities and providing new generating capacity, (3) coal processing for clean fuels to convert the nation's vast coal resources to clean fuels, and (4) industrial applications dependent upon coal use.

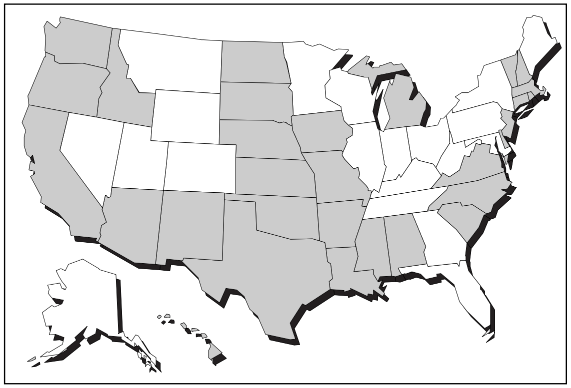
In response to the initial thrust of the program, operations have been completed for 17 of 19 projects that address SO_2 and NO_x control for coal-fired boilers. The resultant technologies provide a suite of cost-effective control options for the full range of boiler types. The 19 environmental control device projects are valued at more than $704 million. These include seven NO_x emission control systems installed in more than 1,750 MWe of utility generating capacity, five SO_2 emissions systems installed on approximately 770 MWe, and seven combined SO_2/NO_x emission control systems installed or planned on more than 665 MWe of capacity.

To respond to load growth as well as growing environmental concerns, the program provides a range of advanced electric power generation options for both repowering and new power generation. These advanced options offer greater than 20 percent reductions in greenhouse gas emissions; SO_2, NO_x, and particulate emissions far below New Source Performance Standards (NSPS); and salable solid and liquid by-products in lieu of solid wastes. Over 1,800 MWe of capacity are represented by 11 projects valued at more than $3.1 billion. These projects include five fluidized-bed combustion (FBC) systems, four integrated gasification combined-cycle (IGCC) systems, and two advanced combustion/heat engine systems. These projects will not only provide environmentally sound electric generation in the late 1990s, but also will provide the demonstrated technology base necessary to meet new capacity requirements in the 21st century.

Also addressed are approaches to converting raw, run-of-mine coals to high-energy-density, low-sulfur products. These products have application domestically for compliance with the Clean Air Act Amendments of 1990 (CAAA). Internationally, both the products and processes have excellent market potential. Valued at more than $519 million, the five projects in the coal processing for clean fuels category represent a diversified portfolio of technologies. Three projects involve the production of high-energy-density solid fuels, one of which also produces a liquid product equivalent to No. 6 fuel oil. A fourth project is demonstrating a new methanol production process. A fifth effort complements the process demonstrations by providing an expert computer software system that enables a utility to assess the environmental, operational, and cost impact of utilizing coals not previously burned at a facility, including upgraded coals and coal blends.

Projects were undertaken as well to address pollution problems associated with coal use in the industrial sector. These included dependence of the steel industry on coke and the inherent pollutant emissions in coke-making; reliance of the cement industry on low-cost indigenous, and often high-sulfur, coal fuels; and the need for many industrial boiler operators to consider switching to coal fuels to reduce operating costs. The five industrial applications projects have a combined value of nearly $1.3 billion. Projects encompass substitution of coal for 40 percent of coke in iron-making, integration of a direct iron-making process with the production of electricity, reduction of cement kiln emissions and solid waste generation, and demonstrations of an industrial-scale slagging combustor and a pulse combustor system.

Section 5 contains a discussion of the technologies being demonstrated and fact sheets for each project.



▲ The CCT projects are spread across the nation in 18 states, indicated in white.

Technology Overview

Environmental Control Devices

Environmental control devices are those technologies applied (retrofitted) to existing or new facilities for the purpose of controlling SO_2 and NO_x emissions. Although boilers may be modified and combustion affected, the basic boiler configuration and function remains unchanged in retrofitting these technologies.

SO_2 Control Technology. Sulfur dioxide is an acid gas formed during coal combustion, which oxidizes the inorganic, pyritic sulfur (Fe_2S), and organically bound sulfur in the coal. Identified as a precursor to formation of acid rain, SO_2 was targeted in Title IV of the CAAA. Phase I of Title IV, effective in 1995, affected 261 coal-fired units nationwide. The required SO_2 reduction was moderate and largely met by switching to low-sulfur fuels. In year 2000, Phase II of Title IV will come into effect, impacting all fossil-fuel-fired units, but most of all, the approximately 900 pre-NSPS coal-fired units. Under the stricter Phase II requirements, compliance by fuel switching alone is unlikely. The CAAA provides utilities flexibility in control strategies through SO_2 allowance trading. This permits a range of control options to be applied by a utility, as well as allowance purchasing. Recognizing this, the CCT Program has sought to provide a portfolio of SO_2 control technologies.

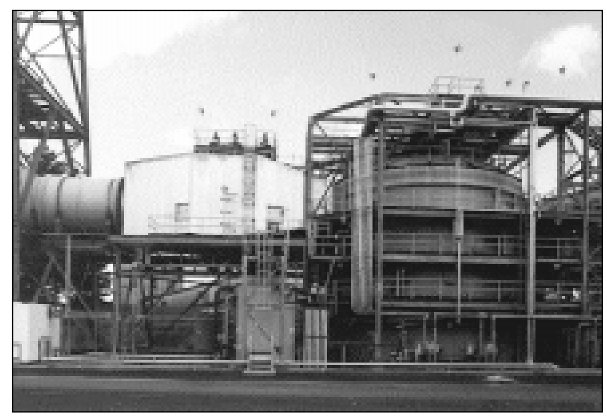
Sulfur dioxide control devices embody those technologies that condition and act upon the flue gas resulting from combustion, not the combustion itself, for the purpose of removing only SO_2. Three basic approaches evolved, driven primarily by different conditions that exist within the pre-NSPS boiler population impacted by the CAAA. There is a tremendous range in critical factors, e.g., size, type, age, and space availability.

On one end of the spectrum are the smaller, older boilers with limited space for adding equipment. For these, sorbent injection techniques hold promise. Sorbent is injected into the boiler or the ductwork, and humidification is incorporated in some fashion to properly condition the flue gas for efficient SO_2 capture. Equipment size and complexity are held to a minimum to keep capital costs and space requirements low. Both limestone and lime sorbents are used. Limestone costs are about one-third that of hydrated lime; but, limestone must be conditioned (calcined), and even then it is less effective in SO_2 capture (under simple sorbent injection conditions) than hydrated lime. Where limestone is used, it is injected in the boiler to produce calcium oxide, which reacts with SO_2 to form solid compounds of calcium sulfite and calcium sulfate. Both limestone and lime injection require the presence of water (humidification) and a calcium-to-sulfur (Ca/S) molar ratio of about 2.0 for sulfur capture efficiencies of 50 to 70 percent.

In the mid-range of the spectrum are 100 to 300 MWe boilers less than 30 years old and somewhat space constrained. For many of these, an increase in front-end control cost is justified by enhanced performance. The approach involves introduction of a reactor vessel in the flue gas stream to create conditions to enhance SO_2 capture beyond that achievable with the simpler sorbent injection systems. Lime, as opposed to limestone, is used and sulfur capture efficiencies up to 90 percent can be achieved at a Ca/S molar ratio of 1.3 to 2.0. This category of control device is called a spray dryer (because the solid by-product from the reaction is dry).

At the other end of the spectrum are the larger (300 MWe and more) boilers with some latitude in space availability, as well as new capacity additions. For these boilers, advanced flue gas desulfurization (AFGD) wet scrubbers, with higher capital cost, but higher sulfur capture efficiency than other approaches, become cost effective. These systems apply larger and somewhat more complex reactors that drive up the capital cost. However, the sorbent is limestone and SO_2 removal efficiencies greater than 90 percent are achieved at a Ca/S molar ratio of about 1.0, making operating costs significantly lower than those of the other two approaches. Furthermore, although the initial AFGD solid by-product is in slurry form, it is dewatered to produce gypsum—a salable product.

Under the CCT Program, two sorbent injection systems, one spray dryer, and two AFGD processes were successfully demonstrated. All have completed testing. Exhibit 5-1 briefly summarizes the characteristics and performance of the technologies that are described in more detail in the project fact sheets.

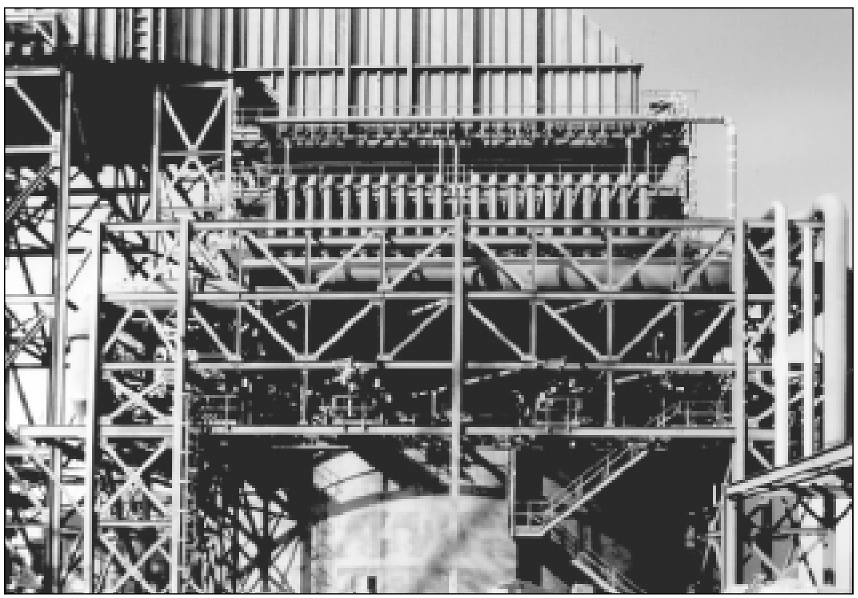


▲ Unique CT-121 SO_2 scrubber at Plant Yates combined a number of functions and eliminated process steps.

Exhibit 5-1
CCT Program SO_2 Control Technology Characteristics

Project	Process	Coal Sulfur Content	SO_2 Reduction	Fact Sheet
Confined Zone Dispersion Flue Gas Desulfurization Demonstration	Sorbent injection—in-duct lime sorbent injection and humidification	1.5–2.5%	50%	5-26
LIFAC Sorbent Injection Desulfurization Demonstration Project	Sorbent injection—furnace sorbent injection (limestone) with vertical humidification vessel and sorbent recycle	2.0–2.9%	70%	5-30
10-MWe Demonstration of Gas Suspension Absorption	Spray dryer—vertical, single-nozzle reactor with integrated sorbent particulate recycle (lime sorbent)	2.7–3.5%	60–90%	5-22
Advanced Flue Gas Desulfurization Demonstration Project	AFGD—co-current flow, integrated quench absorber tower and reaction tank with combined agitation/oxidation (gypsum by-product)	2.25–4.7%	94%	5-34
Demonstration of Innovative Applications of Technology for the CT-121 FGD Process	AFGD—forced flue gas injection into reaction tank (Jet Bubbling Reactor®) for combined SO_2 and particulate capture (gypsum by-product)	1.2–3%	90+%	5-38

▼ This side view of Pure Air's advanced flue gas desulfurization absorber module shows air inlet ducts and sorbent injection piping.



▼ This view shows the sorbent (top) and water (bottom) inlet connections to the Pure Air absorber module.

NO_x Control Technology. Nitrogen oxides (NO_x) are formed from oxidation of nitrogen contained within the coal (fuel-bound NO_x) and oxidation of the nitrogen in the air at high temperatures of combustion (thermal-NO_x). Rapid formation of NO_x at the flame front can occur; but usually, this reaction of hydrocarbon fragments with atmospheric nitrogen represents a small fraction of total NO_x emissions. To control fuel-bound NO_x formation, it is important to limit oxygen at the early stages of combustion. To control thermal-NO_x, it is important to limit peak temperatures.

NO_x was identified both as a precursor to acid rain, targeted under Title IV of the CAAA, and as a contributor to ozone formation, targeted under Title I. Phase I of Title IV, effective in 1995, required some 169 wall- and tangentially-fired coal units to reduce emissions to 0.50 and 0.45 lb/10^6 Btu, respectively. In 2000, Phase II of Title IV will come into effect, impacting all fossil-fueled units, but most of all, the balance of the pre-NSPS coal-fired units (see Exhibit 5-2). Ozone nonattainment prompted the U.S. Environmental Protection Agency to issue a NO_x transport State Implementation Plan (SIP) call for 22 states and the District of Columbia to cut NO_x emissions 85 percent below 1990 rates or achieve a 0.15 lb/10^6 Btu emission rate by May 2003.

The CCT Program has sought to provide a number of NO_x control options to cover the range of boiler types and emission reduction requirements.

Control of NO_x emissions can be accomplished by either modifying the combustion process or acting upon the products of combustion (or combinations thereof). Combustion modification technologies include low-NO_x burners (LNBs), advanced overfire air (AOFA), and reburning processes using either gas or coal. Processes used to act upon flue gas include selective catalytic reduction (SCR) and selective noncatalytic reduction (SNCR).

LNBs regulate the initial fuel-air mixture, velocities, and turbulence to create a fuel-rich flame core and control the rate at which additional air required to complete combustion is mixed. This staging of combustion avoids a highly oxidized environment and hot spots conducive to fuel-NO_x and thermal-NO_x formation. LNBs alone typically can achieve 40 to 50 percent NO_x reduction. But no LNBs have been developed for cyclone-fired boilers.

Exhibit 5-2
Group I and 2 Boiler Statistics and Phase II NO_x Emission Limits

Boiler Types	No. of Boilers	Phase II NO_x Emission Limits (lb/10^6 Btu)
Group 1		
Tangentially fired	299	0.40
Dry-bottom, wall-fired	308	0.46
Group 2		
Cell burner	36	0.68
Cyclone >155 MWe	55	0.86
Wet-bottom, wall-fired >65 MWe	26	0.84
Vertically fired	28	0.80

Source: Environmental Protection Agency, Nitrogen Oxides Emission Reduction Program, Final Rule for Phase II, Group 1 and Group 2 Boilers (downloaded from http://www.epa.gov/docs/acidrain/noxfs3.html).

▲ A portion of ABB Combustion Engineering's Low-NO_x Concentric Firing System (LNCFS™) is shown being installed on a tangentially fired boiler.

AOFA involves injection of air above the primary combustion zone to allow the primary combustion to occur without the amount of oxygen needed for complete combustion. This oxygen deficiency mitigates fuel-NO_x formation. AOFA injected at high velocity creates turbulent mixing to complete the combustion in a gradual fashion at lower temperatures to mitigate thermal-NO_x formation. Usually, AOFA is used in combination with LNBs, but alone, AOFA can achieve 10 to 25 percent NO_x emission reductions. LNB/AOFA systems generally can achieve NO_x emission reductions of 60 to 67 percent.

In reburning, a percentage of the fuel input to the boiler is diverted to injection ports above the primary

Exhibit 5-3
CCT Program NO_x Control Technology Characteristics

Project	Process	Boiler Size/ Type	NO_x Reduction	Fact Sheet
Demonstration of Coal Reburning for Cyclone Boiler NO_x Control	Coal reburning—30% heat input	100-MWe/cyclone	52–62%	5-46
Evaluation of Gas Reburning and Low-NO_x Burners on a Wall-Fired Boiler	LNB/gas reburning/AOFA—13–18% gas heat input	172-MWe/wall	37–65%	5-54
Micronized Coal Reburning Demonstration for NO_x Control	Coal reburning—30% heat input	148-MWe/tangential 50-MWe/cyclone	50–60% (goal)	5-44
Full-Scale Demonstration of Low-NO_x Cell Burner Retrofit	LNB—separation of coal and air ports on plug-in unit	605-MWe/cell burner	48–58%	5-50
Demonstration of Advanced Combustion Techniques for a Wall-Fired Boiler	LNB/AOFA—advanced LNB with separated AOFA and artificial intelligence controls	500-MWe/wall	68%	5-66
180 MWe Demonstration of Advanced Tangentially Fired Combustion Techniques for the Reduction of NO_x Emissions from Coal-Fired Boilers	LNB/AOFA—advanced LNB with close-coupled and separated overfire air	180-MWe/tangential	37–45%	5-62
Demonstration of Selective Catalytic Reduction Technology for the Control of NO_x Emissions from High-Sulfur-Coal-Fired Boilers	SCR—eight catalysts with different shapes and chemical compositions	8.7-MWe/various	80%	5-58

combustion zone. Either gas or coal is typically used as the reburning fuel to provide 10 to 30 percent of the heat input to the boiler. The reburning fuel is injected to create a fuel-rich zone deficient in oxygen (a reducing rather than oxidizing zone). NO_x entering this zone is stripped of oxygen, forming elemental nitrogen. Combustion is completed in a burnout zone where air is injected by an AOFA system. Reburning has application to all boiler types, including cyclone boilers, and can achieve NO_x emission reductions of 50 to 67 percent.

SCR and SNCR can be used alone or in combination with combustion modification. These processes use ammonia or urea in a reducing reaction with NO_x to form elemental nitrogen and water. SNCR can only be used at high temperatures (1,600 to 2,200 ºF) where a catalyst is not needed. SCR is typically applied at temperatures between 600 to 800 ºF. Generally, SNCR and SCR systems alone can achieve NO_x emission reductions of 30 to 50 percent and 80 to 90+ percent, respectively.

Under the CCT Program, seven NO_x control technologies were addressed, encompassing LNBs, AOFA, reburning, SNCR, SCR, and combinations thereof. Six of the projects have completed operations and the remaining one is in the operations phase. Exhibit 5-3 briefly summarizes the characteristics and performance of the technologies that are described in more detail in the project fact sheets.

Combined SO_2/NO_x Control Technology. Combined SO_2/NO_x control systems encompass those technologies that combine previously described control methods and those that apply other, synergistic techniques. Three of the projects combine either LNBs or gas reburning with sorbent injection. In one of these, SNCR is used with LNBs to enhance performance. Another project combines a number of techniques to improve overall system performance, such as LNBs with SNCR, unique space-saving and durable wet-scrubber design, sorbent additive, and artificial intelligence controls. The balance of the seven projects use synergistic methods not previously described.

SO_x-NO_x-Rox Box™ incorporates an SCR catalyst in a high-temperature filter bag for NO_x control and applies sorbent injection for SO_2 control. The high-temperature filter bag, operated in a standard pulsed jet baghouse, protects the SCR catalyst, allows operation at optimal NO_x control temperatures, forms a sorbent cake on the surface to enhance SO_2 capture, and provides high-efficiency particulate capture.

SNOX™ uses SCR followed by catalytic oxidation of SO_2 to SO_3 with condensation of the SO_3 in the presence of water to produce sulfuric acid. Following the SCR with the catalytic oxidation allows the SCR to operate at optimal ammonia concentration without worry of ammonia slip (ammonia passing to the second catalyst is broken down). Furthermore, most particulates passing through the upstream baghouse are captured in the sulfuric acid condensing unit. The system produces no solid waste.

NOXSO uses a single, regenerable adsorber (spherical alumina beads impregnated with sodium carbonate) to capture both SO_2 and NO_x. The adsorber is used in a fluidized bed to achieve effective mixing with the flue gas. The flue gas is then processed through a regenerator system to release the NO_x and SO_2 before return to the fluidized bed.

Six of the seven combined SO_2/NO_x control technology projects have completed operations and one is in the project definition and design phase. Exhibit 5-4 briefly summarizes the characteristics and performance of the technologies that are described in more detail in the project fact sheets.

▲ New York State Electric & Gas Corporation's Milliken Station is hosting the demonstration of a combination of unique SO_2 and NO_x control technologies.

Exhibit 5-4
CCT Program Combined SO_2/NO_x Control Technology Characteristics

Project	Process	Coal Sulfur Content	SO_2/NO_x Reduction	Fact Sheet
LIMB Demonstration Project Extension and Coolside Demonstration	LNB/sorbent injection—furnace and duct injection, calcium-based sorbents	1.6–3.8%	60–70%/40–50%	5-82
Integrated Dry NO_x/SO_2 Emissions Control System	LNB/SNCR/sorbent injection—calcium- and sodium-based sorbents used in duct injection	0.4%	70%/62–80%	5-94
Enhancing the Use of Coals by Gas Reburning and Sorbent Injection	Gas reburning/sorbent injection—calcium-based sorbents used in duct injection	3.0%	50–60%/67%	5-90
Milliken Clean Coal Technology Demonstration Project	LNB/SNCR/wet scrubber—sorbent additive and space-saving, durable scrubber design	1.5–4.0%	98%/53–58%	5-72
SO_x-NO_x-Rox Box™ Flue Gas Cleanup Demonstration Project	SCR/high temperature baghouse/sorbent injection—SCR in high-temperature filter bag and calcium-based sorbent injection	3.4%	80–90%/90%	5-86
SNOX™ Flue Gas Cleaning Demonstration Project	SCR/oxidation catalyst/sulfuric acid condenser—synergistic catalyst effect and no solid waste	3.4%	95%/94%	5-78
Commercial Demonstration of the NOXSO SO_2/NO_x Removal Flue Gas Cleanup System	Regenerable adsorbent—spherical alumina beads impregnated with sodium carbonate in fluidized-bed adsorber	3.4% (planned)	98% (goal)/75% (goal)	5-76

Advanced Electric Power Generation Technology

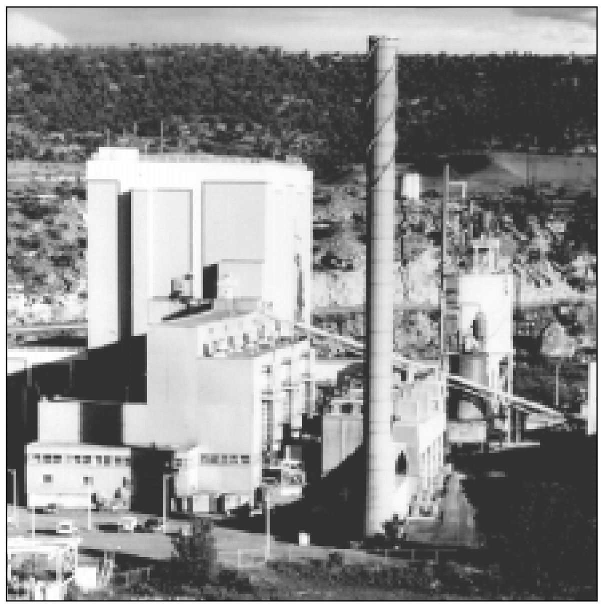
Advanced electric power generation technologies enable the efficient and environmentally superior generation of electricity. The advanced electric power generation projects selected under the CCT Program are responsive to the capacity expansion needs requisite to meeting long-term demand, offsetting nuclear retirements, and meeting stringent CAAA emission limits effective in 2000. These technologies are characterized by high thermal efficiency, very low pollutant emissions, reduced CO_2 emissions, few solid waste problems, and enhanced economics. Advanced electric power generation technologies may be deployed in modules, allowing phased construction to better match demand growth, and to meet the smaller capacity requirements of municipal, rural, and nonutility generators.

There are five generic advanced electric power generation technologies demonstrated in the CCT Program. The characteristics of these five technologies are outlined here, and the specific projects and technologies are presented in more detail in the fact sheets.

Fluidized-Bed Combustion. Fluidized-bed combustion (FBC) reduces emissions of SO_2 and NO_x by controlling combustion parameters and by injecting a sorbent (such as crushed limestone) into the combustion chamber along with the coal. Pulverized coal mixed with the limestone is fluidized on jets of air in the combustion chamber. Sulfur released from the coal as SO_2 is captured by the sorbent in the bed to form a solid calcium compound that is removed with the ash. The resultant waste is a dry, benign solid that can be disposed of easily or used in agricultural and construction applications. More than 90 percent of the SO_2 can be captured this way.

At combustion temperatures of 1,400 to 1,600 ºF, the fluidized mixing of the fuel and sorbent enhances both combustion and sulfur capture. The operating temperature range is about half that of a conventional pulverized-coal boiler and below the temperature at which thermal NO_x is formed. In fact, fluidized-bed NO_x emissions are about 70 to 80 percent lower than those for conventional pulverized-coal boilers. Thus, fluidized-bed combustors substantially reduce both SO_2 and NO_x emissions. Also, fluidized-bed combustion has the capability of using high-ash coal, whereas conventional pulverized-coal units must limit ash content in the coal to relatively low levels.

Two parallel paths were pursued in fluidized-bed development—bubbling and circulating beds. Bubbling beds use a dense fluid bed and low fluidization velocity to effect good heat transfer and mitigate erosion of an in-bed heat exchanger. Circulating fluidized beds use a relatively high fluidization velocity, which entrains the bed material, in conjunction with hot cyclones to separate and recirculate the bed material from the flue gas before it passes to a heat exchanger. Hybrid systems have also evolved from these two basic approaches.



▲ Tri-State Generation and Transmission Association's Nucla Station was host to demonstration of the world's first utility-scale AFBC.

Fluidized-bed combustion can be either atmospheric (AFBC) or pressurized (PFBC). AFBC operates at atmospheric pressure while PFBC operates at pressure 6 to 16 times higher. PFBC offers potentially higher efficiency, and consequently, reduced operating costs and waste relative to AFBC.

Second-generation PFBC integrates the combustor with a pyrolyzer (coal gasifier) to fuel a gas turbine (topping cycle), the waste heat from which is used to generate steam for a steam turbine (bottoming cycle). The inherent efficiency of the gas turbine and waste heat recovery in this combined-cycle mode significantly increases overall efficiency. Such advanced PFBC systems have the potential for efficiencies over 50 percent.

Integrated Gasification Combined Cycle. The integrated coal gasification combined-cycle process has four basic steps: (1) fuel gas is generated from coal reacting with high-temperature steam and an oxidant (oxygen or air) in a reducing atmosphere; (2) the fuel gas is either passed directly to a hot-gas cleanup system to remove particulates, sulfur, and nitrogen compounds or first cooled to produce steam and then cleaned conventionally; (3) the clean fuel gas is combusted in a gas turbine generator to produce electricity; and (4) the residual heat in the hot exhaust gas from the gas turbine is recovered in a heat recovery steam generator, and the steam is used to produce additional electricity in a steam turbine generator.

Integrated gasification combined-cycle (IGCC) systems are among the cleanest and most efficient of the emerging clean coal technologies. Sulfur, nitrogen compounds, and particulates are removed before the fuel is burned in the gas turbine, that is, before combustion air is added. For this reason, there is a much lower volume of gas to be treated than in a postcombustion scrubber. The chemical composition of the gas requires that the gas stream must be cleaned to a high degree, not only to achieve low emissions, but to protect downstream components, such as the gas turbine, from erosion and corrosion.

In a coal gasifier, the sulfur in the coal is released in the form of hydrogen sulfide (H_2S) rather than as SO_2, which is the case in conventional pulverized-coal combustion. In some IGCC systems, much of the sulfur-containing gas is captured by a sorbent injected into the gasifier. Others use existing proven commercial hydrogen sulfide removal processes, which remove up to 99+ percent of the sulfur, but require the fuel to be cooled, which is an efficiency penalty. Therefore, hot-gas cleanup systems are now being demonstrated. In these cleanup systems, the hot coal gas is passed through a bed of metal oxide particles, such as supported zinc oxides. Zinc oxide can absorb sulfur contaminants at temperatures in excess of 1,000 ºF, and the compound can be regenerated and reused with little loss of effectiveness. Produced during the regeneration stage are salable sulfur, sulfuric acid, or sulfur-containing solid waste, which may be used to produce useful by-products, such as gypsum. The technique is capable of removing more than 99.9 percent of the sulfur in the gas stream. With hot-gas cleanup, IGCC systems have the potential for efficiencies of over 50 percent.

High levels of nitrogen removal are also possible. Some of the coal's nitrogen is converted to ammonia, which can be almost totally removed by commercially available chemical processes. NO_x formed in the gas turbine can be held to well within allowable levels by staged combustion in the gas turbine or by adding moisture to control flame temperature.

Integrated Gasification Fuel Cell. A typical fuel cell system using coal as fuel includes a coal gasifier with a gas cleanup system, a fuel cell to use the coal gas to generate electricity (direct current) and heat, an inverter to convert direct current to alternating current, and a heat-recovery system. The heat-recovery system would be used to produce additional electric power in a bottoming steam cycle.

▲ Tampa Electric Company's Polk Power Station Unit 1, a 250-MWe IGCC greenfield installation, is currently in operation. It is one of the world's cleanest and most advanced coal power plants.

Energy conversion in fuel cells is potentially more efficient (up to 60 percent, depending on fuel and type of fuel cell) than traditional energy conversion devices. Fuel cells directly transform the chemical energy of a fuel and an oxidant (air or oxygen) into electrical energy instead of going through an intermediate step, i.e., burner, boiler, turbines, and generators. Each fuel cell includes an anode and a cathode separated by an electrolyte layer. In a typical fuel cell, coal gas is supplied to the anode and air is supplied to the cathode to produce electricity and heat.

Coal-Fired Diesel. Either a coal-oil or coal-water slurry fuels a diesel-engine, which drives an electric generation system. The hot exhaust from the diesel engine is routed through a heat-recovery unit to produce steam for a steam-turbine electric generating system (combined cycle). Environmental control systems for SO_2, NO_x, and particulate removal treat the cooled exhaust before release to the atmosphere. The diesel system is expected to achieve 45 to 48 percent thermal efficiencies. The 10 to 100 MWe capacity range of the technology would be most applicable to small utilities, municipalities, rural cooperatives, and industrial cogeneration.

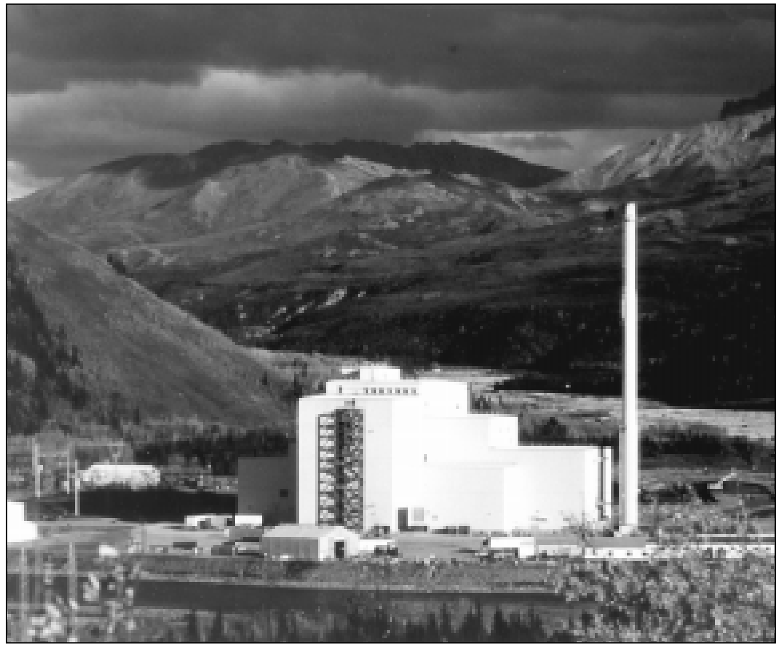
Slagging Combustor. Many new coal-burning technologies are designed to remove the coal ash as molten slag in the combustor rather than the furnace. Most of these slagging combustors are based on a cyclone combustor concept. In a cyclone combustor, coal is burned in a separate chamber outside the furnace cavity. The hot combustion gases then pass into the boiler where the actual heat exchange takes place.

The advantage of a cyclone combustor is that the ash is kept out of the furnace cavity where it could collect on boiler tubes and lower heat transfer efficiency. To keep ash from being blown into the furnace, the combustion temperature is kept so hot that mineral impurities melt and form slag, hence the name slagging combustor. A vortex of air (the cyclone) forces the slag to the outer walls of the combustor where it can be removed as waste. Because ash removal efficiency is high, there is no degradation of boiler tube surfaces to reduce boiler efficiency over time.

Results to date show that by positioning air injection ports so that coal is combusted in stages, NO_x emissions can be reduced by 70 to 80 percent. Injecting limestone into the combustion chamber has the potential to reduce sulfur emissions by 90 percent in combination with a spray-dryer absorber. Advanced slagging combustors could replace oil-fired units in both utility and industrial applications or be used to retrofit older, conventional cyclone boilers.

Status of Projects. There are 11 advanced electric power generating projects in the CCT Program of which five are fluidized-bed combustion systems, four are IGCCs, one is a coal diesel, and one is an advanced slagging combustor. Of the five fluidized-bed combustion projects, two have successfully completed demonstration (one PFBC and one AFBC), and the other three are in the project definition and design phase. Of the four IGCC projects, three are in operation and one is in the project definition and design phase. Of the two remaining projects, operation was initiated in January 1998 on the advanced slagging combustor project, and the coal diesel project is in the project definition and design phase.

Exhibit 5-5 summarizes the process characteristics and size of the advanced electric power generating technologies presented in more detail in the project fact sheets.



▲ Golden Valley Electric Association is adding capacity to its 25 MWe Healy Unit No. 1 with a 50-MWe slagging combustor unit using 65 percent waste coal.

Exhibit 5-5
CCT Program Advanced Electric Power Generation Technology Characteristics

Project	Process	Size	Fact Sheet
Fluidized-Bed Combustion			
McIntosh Unit 4A PCFB Demonstration Project	Pressurized circulating fluidized-bed combustion	145-MWe	5-100
McIntosh Unit 4B Topped PCFB Demonstration Project	McIntosh 4A with pyrolyzer and topping combustor	145-MWe + 93-MWe	5-102
Tidd PFBC Demonstration Project	Pressurized bubbling fluidized-bed combustion	70-MWe	5-106
JEA Large-Scale CFB Combustion Demonstration Project	Atmospheric circulating fluidized-bed combustion	297.5-MWe	5-104
Nucla CFB Demonstration Project	Atmospheric circulating fluidized-bed combustion	100-MWe	5-110
Integrated Gasification Combined Cycle			
Clean Energy Demonstration Project	Oxygen-blown, slagging fixed-bed gasifier with cold gas cleanup, fuel cell slipstream	477-MWe	5-116
Piñon Pine IGCC Power Project	Air-blown, fluidized-bed gasifier with hot gas cleanup	99-MWe	5-118
Tampa Electric Integrated Gasification Combined-Cycle Project	Oxygen-blown, entrained-flow gasifier with hot and cold gas cleanup	250-MWe	5-120
Wabash River Coal Gasification Repowering Project	Oxygen-blown, two-stage entrained-flow gasifier with cold gas cleanup	262-MWe	5-122
Advanced Combustion/Heat Engines			
Healy Clean Coal Project	Advanced slagging combustor, spray dryer with sorbent recycle	50-MWe	5-126
Clean Coal Diesel Demonstration Project	Coal-fueled diesel engine	6.4-MWe	5-128

Coal Processing for Clean Fuels Technology

The coal processing category includes a range of technologies designed to produce high-energy-density, low-sulfur solid and clean liquid fuels, as well as systems to assist users in evaluating impacts of coal quality on boiler performance.

In the case of the Customs Coals International project, advanced physical-cleaning techniques are applied to bituminous coal with an already high Btu content to remove the ash, which contains sulfur in the form of pyrite, an inorganic iron compound. A dense-medium cyclone using finely sized magnetite effectively separates 90 percent of the pyritic sulfur. But, because physical methods cannot remove the organically bound sulfur, dense-medium-cyclone processed coals can only be considered compliance coals (meeting CAAA SO_2 requirements) if the organic sulfur content is very low. This processed compliance coal is called Carefree Coal™. For coals with significant organic sulfur content, sorbents and other additives must be added to capture the sulfur released upon combustion and bring the coal into compliance. This second product is called Self-Scrubbing Coal™. The project is on hold pending resolution of financial matters.

The Rosebud SynCoal Partnership's advanced coal conversion project applies mostly physical-cleaning methods to low-Btu, low-sulfur subbituminous coals, primarily to remove moisture and secondarily to remove ash. The objective is to enhance the energy density of the already low-sulfur coal. Some conversion of the surface properties of the coal is required, however, to provide stability (prevent spontaneous combustion) in transport and handling. In the process, coal with 5,500 to 9,000 Btu/lb, 25 to 40 percent moisture content, and 0.5 to 1.5 percent sulfur is converted to a 12,000 Btu/lb product with 1.0 percent moisture and as low as 0.3 percent sulfur. Test burning of processed coal at utilities is continuing.

The ENCOAL project, which completed operational testing in July 1997, has used mild gasification to convert low-Btu, low-sulfur subbituminous coal to a high-energy-density, low-sulfur solid product and a clean liquid fuel comparable to No. 6 fuel oil. Mild gasification is a pyrolysis process (heating in the absence of oxygen) performed at moderate temperatures and pressures. It produces condensable volatile hydrocarbons in addition to solids and gas. The condensable fraction is drawn off as a liquid product. Most of the gas is used to provide on-site energy requirements. The process solid is significantly beneficiated to produce a 11,000-Btu/lb low-sulfur solid fuel. The demonstration plant processed 500 tons per day of subbituminous coal and produced 250 tons per day of solid Process-Derived Fuel (PDF®) and 250 barrels per day of Coal-Derived Liquids (CDL®). Both the solid and liquid fuels have undergone test burns at utility and industrial sites. The project was successfully completed in December 1997.

The liquid-phase methanol (LPMEOH™) process being demonstrated is an indirect liquefaction process using synthesis gas from a coal gasifier. The unique aspect of the process is the use of an inert liquid to suspend the conversion catalyst. This removes the heat of reaction and precludes the need for an intermediate water-gas shift conversion. Also addressed in the project are the load-following capability of the process by simulating application in an IGCC system and fuel characteristics of the unrefined product. Construction on the project was completed in January 1997. Operation began in April 1997.

CQ Inc. has developed a personal computer software package that will serve as a predictive tool to assist utilities in selecting optimal quality coal for a specific boiler based on operational efficiency, cost, and environmental considerations. Algorithms were developed and verified through comparative testing at bench, pilot, and utility scale. Six large-scale field tests were conducted at five separate utilities. The software has been released for use.

Exhibit 5-6 summarizes the process characteristics and size of the coal processing for clean fuels technologies presented in more detail in the project fact sheets.

Exhibit 5-6
CCT Program Coal Processing for Clean Fuels Technology Characteristics

Project	Process	Size	Fact Sheet
Development of the Coal Quality Expert™	Coal Quality Expert™ computer software	Tested at 250–880-MWe	5-138
Advanced Coal Conversion Process Demonstration	Advanced coal conversion process for upgrading low-rank coals	45 tons/hr	5-136
ENCOAL® Mild Gasification Project	Liquids-from-coal (LFC®) mild gasification to produce solid and liquid fuels	1,000 tons/day	5-142
Commercial-Scale Demonstration of the Liquid-Phase Methanol (LPMEOH™) Process	Liquid phase process for methanol production from coal-derived syngas	80,000 gal/day	5-132
Self-Scrubbing Coal™: An Integrated Approach to Clean Air	Dense-medium cyclones with finely sized magnetic and sorbent addition for bituminous coals	500 tons/hr	5-134

▼ Rosebud SynCoal Partnership's advanced coal conversion process plant in Colstrip, MT, has produced over a million tons of SynCoal® products.

▼ The ENCOAL® mild gasification plant near Gillette, WY, has operated 12,800 hours and processed approximately 247,000 tons of raw coal.

▼ The LPMEOH™ process produces over 80,000 gal/day of methanol, all of which is used by the Eastman Chemical Company.

Industrial Applications Technology

Technologies applicable to the industrial sector address significant environmental issues and barriers associated with coal use in industrial processes. These technologies are directed at both continued coal use and introduction of coal use in various industrial sectors.

One of the critical environmental concerns has to do with pollutant emissions resulting from producing coke from coal in steelmaking. Two approaches to mitigate or eliminate this problem are being demonstrated. In one, about 40 percent of the coke is displaced through direct injection of granular coal into a blast furnace system. The coal is essentially burned in the blast furnace where the pollutant emissions are readily controlled (as opposed to first coking the coal). The other approach precludes the need for coke making by using a direct iron-making process, HIsmelt®. In this process, raw coal is introduced into a melter-gasifier to produce reducing gas and heat for a unique reduction furnace; no coke is required. Excess reducing gas is cleaned and used to fuel a boiler for electric power generation.

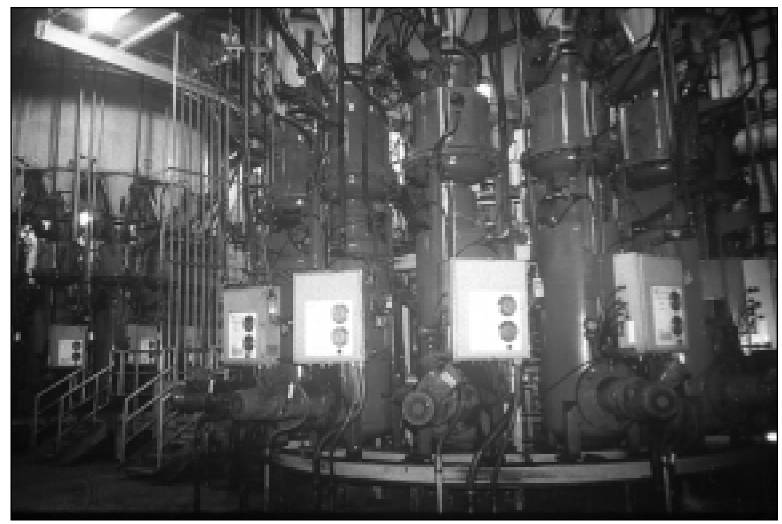
Because production costs are largely driven by fuel cost, coal is often the fuel of choice in cement production. Faced with the need to control SO_2 emissions and also to address growing solid waste management problems, industry sponsored the demonstration of an innovative SO_2 scrubber. The successfully demonstrated Passamaquoddy Technology Recovery Scrubber™ uses cement kiln dust, otherwise discarded as waste, to control SO_2 emissions, convert the sulfur and chloride acid gases to fertilizer, return the solid by-product as cement kiln feedstock, and produce distilled water. No new wastes are generated and cement kiln dust waste is converted to feedstock. This technology also has application for controlling pollutant emissions in paper production and waste-to-energy applications.

In many industrial boiler applications, the relatively low, stable price of coal makes it an attractive substitute for oil and gas feedstock. However, drawbacks to conversion of oil- and gas-fired units to coal include addition of SO_2 and NO_x controls, tube fouling, and the need for a coolant water circuit for the combustor. Oil- and gas-fired units are not high SO_2 or NO_x emitters, use relatively tight tube spacing in the absence of the potential for ash fouling, and the flow of oil or gas cools the combustor, precluding the need for water cooling. For these reasons, the CCT Program demonstrated an advanced air-cooled, slagging combustor that could avoid these potential problems. The cyclone combustor stages introduction of air to control NO_x, injects sorbent to control SO_2, slags the ash in the combustor to prevent tube fouling, and uses air cooling to preclude the need for water circuitry.

A pulse combustor being demonstrated by ThermoChem has a wide range of applications. The technology can be used in many coal processes, including coal gasification, as well as waste-to-energy applications.

The cement kiln and slagging combustor projects are completed. The project demonstrating granular-coal

▲ Shown here is the completed Bethlehem Steel Corporation facility to demonstrate the injection of granulated coal directly into two blast furnaces at Burns Harbor, IN.



▲ Shown here is the granular-coal injection system.

Exhibit 5-7
CCT Program Industrial Applications Technology Characteristics

Project	Process	Size	Fact Sheet
Blast Furnace Granular-Coal Injection System Demonstration Project	Blast furnace granular-coal injection for reduction of coke use	7,000 net tons/day of hot metal/furnace per day	5-148
Advanced Cyclone Combustor with Internal Sulfur, Nitrogen, and Ash Control	Advanced slagging combustor with staged combustion and sorbent injection	23 x 10^6 Btu/hr	5-152
Clean Power from Integrated Coal/Ore Reduction (CPICOR™)	HIsmelt® direct reduction iron-making process to eliminate coke; combined-cycle power generation	195-MWe 3,300 tons/day of hot metal	5-150
Cement Kiln Flue Gas Recovery Scrubber	Cement kiln dust used to capture SO_2; dust converted to feedstock; and fertilizer and distilled water produced	1,450 tons/day of cement	5-156
Pulse Combustor Design Qualification Test	Advanced combustion using Manufacturing and Technology Conversion International's pulse combustor/gasifier	To be determined	5-160

injection into a blast furnace is in operation. Demonstration of the HIsmelt® direct iron-making process and the ThermoChem project are in the project definition and design phase.

Exhibit 5-7 summarizes process characteristics and size for the industrial applications technologies presented in more detail in the project fact sheets.

Project Fact Sheets

The remainder of this section contains fact sheets for all 40 projects. Two types of facts sheets are provided: (1) a brief, two page overview for ongoing projects and (2) an expanded four page summary for projects that have successfully completed operational testing. The expanded fact sheets for completed projects contain a summary of the major results from the demonstration as well as sources for obtaining further information, specifically, contact persons and key references. Information provided in the fact sheets includes the project participant and team members, project objectives, significant project features, process description, major milestones, progress (if ongoing) or summary of results (if completed), and commercial applications. A key to interpreting the milestone charts is provided on the right. To prevent the release of project-specific information of a proprietary nature, process flow diagrams contained in the fact sheets are highly simplified and presented only as illustrations of the concepts involved in the demonstrations. The portion of the process or facility central to the demonstration is demarcated by the shaded area.

An index to project fact sheets is provided in Exhibit 5-8. Projects are listed by application category. Ongoing projects in each category appear first followed by projects having completed operations. A shaded area distinguishes projects having completed operations from ongoing projects. Within these breakdowns, projects are listed alphabetically by participant. In addition, Exhibit 5-8 indicates the solicitation under which the project was selected; its status as of September 30, 1998; and the page number for each Fact Sheet. Exhibit 5-9 lists the projects alphabetically by participant and provides project location and page numbers.

Key to Milestone Charts in Fact Sheets

Each fact sheet contains a bar chart that highlights major milestones—past and planned. The bar chart shows a project's duration and indicates the time period for three general categories of project activities—preaward, design and construction, and operation. The key provided below explains what is included in each of these categories.

Preaward

Includes preaward briefings, negotiations, and other activities conducted during the period between DOE's selection of the project and award of the cooperative agreement.

Design and Construction

Includes the NEPA process, permitting, design, procurement, construction, preoperational testing, and other activities conducted prior to the beginning of operation of the demonstration.

MTF Memo-to-file

CX Categorical exclusion

EA Environmental assessment

EIS Environmental impact statement

Operation

Begins with start-up of operation and includes operational testing, data collection, analysis, evaluation, reporting, and other activities to complete the demonstration project.

Exhibit 5-8
Project Fact Sheets by Application Category

Project	Participant	Solicitation/Status	Page
Environmental Control Devices			
SO_2 Control Technologies			
10-MWe Demonstration of Gas Suspension Absorption	AirPol, Inc.	CCT-III/completed 3/94	5-22
Confined Zone Dispersion Flue Gas Desulfurization Demonstration	Bechtel Corporation	CCT-III/completed 6/93	5-26
LIFAC Sorbent Injection Desulfurization Demonstration Project	LIFAC–North America	CCT-III/completed 6/94	5-30
Advanced Flue Gas Desulfurization Demonstration Project	Pure Air on the Lake, L.P.	CCT-II/completed 6/95	5-34
Demonstration of Innovative Applications of Technology for the CT-121 FGD Process	Southern Company Services, Inc.	CCT-II/completed 12/94	5-38
NO_x Control Technologies			
Micronized Coal Reburning Demonstration for NO_x Control	New York State Electric & Gas Corporation	CCT-IV/operational	5-44
Demonstration of Coal Reburning for Cyclone Boiler NO_x Control	The Babcock & Wilcox Company	CCT-II/completed 12/92	5-46
Full-Scale Demonstration of Low-NO_x Cell Burner Retrofit	The Babcock & Wilcox Company	CCT-III/completed 4/93	5-50
Evaluation of Gas Reburning and Low-NO_x Burners on a Wall-Fired Boiler	Energy and Environmental Research Corporation	CCT-III/completed 1/95	5-54
Demonstration of Selective Catalytic Reduction Technology for the Control of NO_x Emissions from High-Sulfur-Coal-Fired Boilers	Southern Company Services, Inc.	CCT-II/completed 7/95	5-58
180-MWe Demonstration of Advanced Tangentially Fired Combustion Techniques for the Reduction of NO_x Emissions from Coal-Fired Boilers	Southern Company Services, Inc.	CCT-II/completed 12/92	5-62
Demonstration of Advanced Combustion Techniques for a Wall-Fired Boiler	Southern Company Services, Inc.	CCT-II/completed 5/98	5-66
Combined SO_2/NO_x Control Technologies			
Commercial Demonstration of the NOXSO SO_2/NO_x Removal Flue Gas Cleanup System	NOXSO Corporation	CCT-III/design	5-76
SNOX™ Flue Gas Cleaning Demonstration Project	ABB Environmental Systems	CCT-II/completed 12/94	5-78
LIMB Demonstration Project Extension and Coolside Demonstration	The Babcock & Wilcox Company	CCT-I/completed 8/91	5-82
SO_x-NO_x-Rox Box™ Flue Gas Cleanup Demonstration Project	The Babcock & Wilcox Company	CCT-II/completed 5/93	5-86
Enhancing the Use of Coals by Gas Reburning and Sorbent Injection	Energy and Environmental Research Corporation	CCT-I/completed 10/94	5-90
Milliken Clean Coal Technology Demonstration Project	New York State Electric & Gas Corporation	CCT-IV/completed 6/98	5-72
Integrated Dry NO_x/SO_2 Emissions Control System	Public Service Company of Colorado	CCT-III/completed 12/96	5-94
Advanced Electric Power Generation			
Fluidized-Bed Combustion			
McIntosh Unit 4A PCFB Demonstration Project	City of Lakeland, Lakeland Electric	CCT-III/design	5-100
McIntosh Unit 4B Topped PCFB Demonstration Project	City of Lakeland, Lakeland Electric	CCT-V/design	5-102
JEA Large Scale CFB Combustion Demonstration Project	JEA	CCT-I/design	5-104

Shaded area indicates projects having completed operations.

Exhibit 5-8 (continued)
Project Fact Sheets by Application Category

Project	Participant	Solicitation/Status	Page
Tidd PFBC Demonstration Project	The Ohio Power Company	CCT-I/completed 3/95	5-106
Nucla CFB Demonstration Project	Tri-State Generation and Transmission Association, Inc.	CCT-I/completed 1/91	5-110
Integrated Gasification Combined Cycle			
Clean Energy Demonstration Project	Clean Energy Partners Limited Partnership	CCT-V/design	5-116
Piñon Pine IGCC Power Project	Sierra Pacific Power Company	CCT-IV/operational	5-118
Tampa Electric Integrated Gasification Combined-Cycle Project	Tampa Electric Company	CCT-III/operational	5-120
Wabash River Coal Gasification Repowering Project	Wabash River Coal Gasification Repowering Project Joint Venture	CCT-IV/operational	5-122
Advanced Combustion/Heat Engines			
Healy Clean Coal Project	Alaska Industrial Development and Export Authority	CCT-III/operational	5-126
Clean Coal Diesel Demonstration Project	Arthur D. Little, Inc.	CCT-V/construction	5-128
Coal Processing for Clean Fuels			
Commercial-Scale Demonstration of the Liquid-Phase Methanol (LPMEOH™) Process	Air Products Liquid Phase Conversion Company, L.P.	CCT-III/operational	5-132
Self-Scrubbing Coal™: An Integrated Approach to Clean Air	Custom Coals International	CCT-IV/design	5-134
Advanced Coal Conversion Process Demonstration	Rosebud SynCoal Partnership	CCT-I/operational	5-136
Development of the Coal Quality Expert™	ABB Combustion Engineering, Inc., and CQ Inc.	CCT-I/completed 12/95	5-138
ENCOAL Mild Coal Gasification Project	ENCOAL® Corporation	CCT-III/completed 7/97	5-142
Industrial Applications			
Blast Furnace Granular-Coal Injection System Demonstration Project	Bethlehem Steel Corporation	CCT-III/operational	5-148
Clean Power from Integrated Coal/Ore Reduction (CPICOR™)	CPICOR™ Management Company, L.L.C.	CCT-V/design	5-150
Pulse Combustor Design Qualification Test	ThermoChem, Inc.	CCT-IV/design	5-160
Advanced Cyclone Combustor with Internal Sulfur, Nitrogen, and Ash Control	Coal Tech Corporation	CCT-I/completed 5/90	5-152
Cement Kiln Flue Gas Recovery Scrubber	Passamaquoddy Tribe	CCT-II/completed 9/93	5-156

Shaded area indicates projects having completed operations.

Exhibit 5-9
Project Fact Sheets by Participant

Participant	Project	Location	Page
ABB Combustion Engineering, Inc., and CQ Inc.	Development of the Coal Quality Expert™	Homer City, PA	5-138
ABB Environmental Systems	SNOX™ Flue Gas Cleaning Demonstration Project	Niles, OH	5-78
Air Products Liquid Phase Conversion Company, L.P.	Commercial-Scale Demonstration of the Liquid-Phase Methanol (LPMEOH™) Process	Kingsport, TN	5-132
AirPol, Inc.	10-MWe Demonstration of Gas Suspension Absorption	West Paducah, KY	5-22
Alaska Industrial Development and Export Authority	Healy Clean Coal Project	Healy, AK	5-126
Arthur D. Little, Inc.	Clean Coal Diesel Demonstration Project	Fairbanks, AK	5-128
The Babcock & Wilcox Company	Demonstration of Coal Reburning for Cyclone Boiler NO_x Control	Cassville, WI	5-46
The Babcock & Wilcox Company	Full-Scale Demonstration of Low-NO_x Cell Burner Retrofit	Aberdeen, OH	5-50
The Babcock & Wilcox Company	LIMB Demonstration Project Extension and Coolside Demonstration	Lorain, OH	5-82
The Babcock & Wilcox Company	SO_x-NO_x-Rox Box™ Flue Gas Cleanup Demonstration Project	Dilles Bottom, OH	5-86
Bechtel Corporation	Confined Zone Dispersion Flue Gas Desulfurization Demonstration	Seward, PA	5-26
Bethlehem Steel Corporation	Blast Furnace Granular-Coal Injection System Demonstration Project	Burns Harbor, IN	5-148
City of Lakeland, Lakeland Electric	McIntosh Unit 4A PCFB Demonstration Project	Lakeland, FL	5-100
City of Lakeland, Lakeland Electric	McIntosh Unit 4B Topped PCFB Demonstration Project	Lakeland, FL	5-102
Clean Energy Partners Limited Partnership	Clean Energy Demonstration Project	Grand Tower, IL	5-116
Coal Tech Corporation	Advanced Cyclone Combustor with Internal Sulfur, Nitrogen, and Ash Control	Williamsport, PA	5-152
CPICOR™ Management Company, L.L.C.	Clean Power from Integrated Coal/Ore Reduction (CPICOR™)	Vineyard, UT	5-150
Custom Coals International	Self-Scrubbing Coal™: An Integrated Approach to Clean Air	Central City, PA	5-134
ENCOAL® Corporation	ENCOAL® Mild Coal Gasification Project	Gillette, WY	5-142
Energy and Environmental Research Corporation	Enhancing the Use of Coals by Gas Reburning and Sorbent Injection	Hennepin, IL Springfield, IL	5-90
Energy and Environmental Research Corporation	Evaluation of Gas Reburning and Low-NO_x Burners on a Wall-Fired Boiler	Denver, CO	5-54
JEA	JEA Large-Scale CFB Combustion Demonstration Project	Jacksonville, FL	5-104
LIFAC–North America	LIFAC Sorbent Injection Desulfurization Demonstration Project	Richmond, IN	5-30
New York State Electric & Gas Corporation	Micronized Coal Reburning Demonstration for NO_x Control	Lansing, NY	5-44

Exhibit 5-9 (continued)
Project Fact Sheets by Participant

Participant	Project	Location	Page
New York State Electric & Gas Corporation	Milliken Clean Coal Technology Demonstration Project	Lansing, NY	5-72
NOXSO Corporation	Commercial Demonstration of the NOXSO SO_2/NO_x Removal Flue Gas Cleanup System	To be determined	5-76
The Ohio Power Company	Tidd PFBC Demonstration Project	Brilliant, OH	5-106
Passamaquoddy Tribe	Cement Kiln Flue Gas Recovery Scrubber	Thomaston, ME	5-156
Public Service Company of Colorado	Integrated Dry NO_x/SO_2 Emissions Control System	Denver, CO	5-94
Pure Air on the Lake, L.P.	Advanced Flue Gas Desulfurization Demonstration Project	Chesterton, IN	5-30
Rosebud SynCoal Partnership	Advanced Coal Conversion Process Demonstration	Colstrip, MT	5-136
Sierra Pacific Power Company	Piñon Pine IGCC Power Project	Reno, NV	5-118
Southern Company Services, Inc.	Demonstration of Advanced Combustion Techniques for a Wall-Fired Boiler	Coosa, GA	5-66
Southern Company Services, Inc.	Demonstration of Innovative Applications of Technology for the CT-121 FGD Process	Newnan, GA	5-38
Southern Company Services, Inc.	Demonstration of Selective Catalytic Reduction Technology for the Control of NO_x Emissions from High-Sulfur-Coal-Fired Boilers	Pensacola, FL	5-58
Southern Company Services, Inc.	180-MWe Demonstration of Advanced Tangentially Fired Combustion Techniques for the Reduction of NO_x Emissions from Coal-Fired Boilers	Lynn Haven, FL	5-62
Tampa Electric Company	Tampa Electric Integrated Gasification Combined-Cycle Project	Mulberry, FL	5-150
ThermoChem, Inc.	Pulse Combustor Design Qualification Test	Baltimore, MD	5-160
Tri-State Generation and Transmission Association, Inc.	Nucla CFB Demonstration Project	Nucla, CO	5-110
Wabash River Coal Gasification Repowering Project Joint Venture	Wabash River Coal Gasification Repowering Project	West Terre Haute, IN	5-122

Environmental Control Devices
SO_2 Control Technology

10-MWe Demonstration of Gas Suspension Absorption

Project completed.

Participant
AirPol, Inc.

Additional Team Members
FLS miljo, Inc. (FLS) —technology owner
Tennessee Valley Authority—cofunder and site owner

Location
West Paducah, McCracken County, KY

Technology
FLS' Gas Suspension Absorption (GSA) system for flue gas desulfurization (FGD)

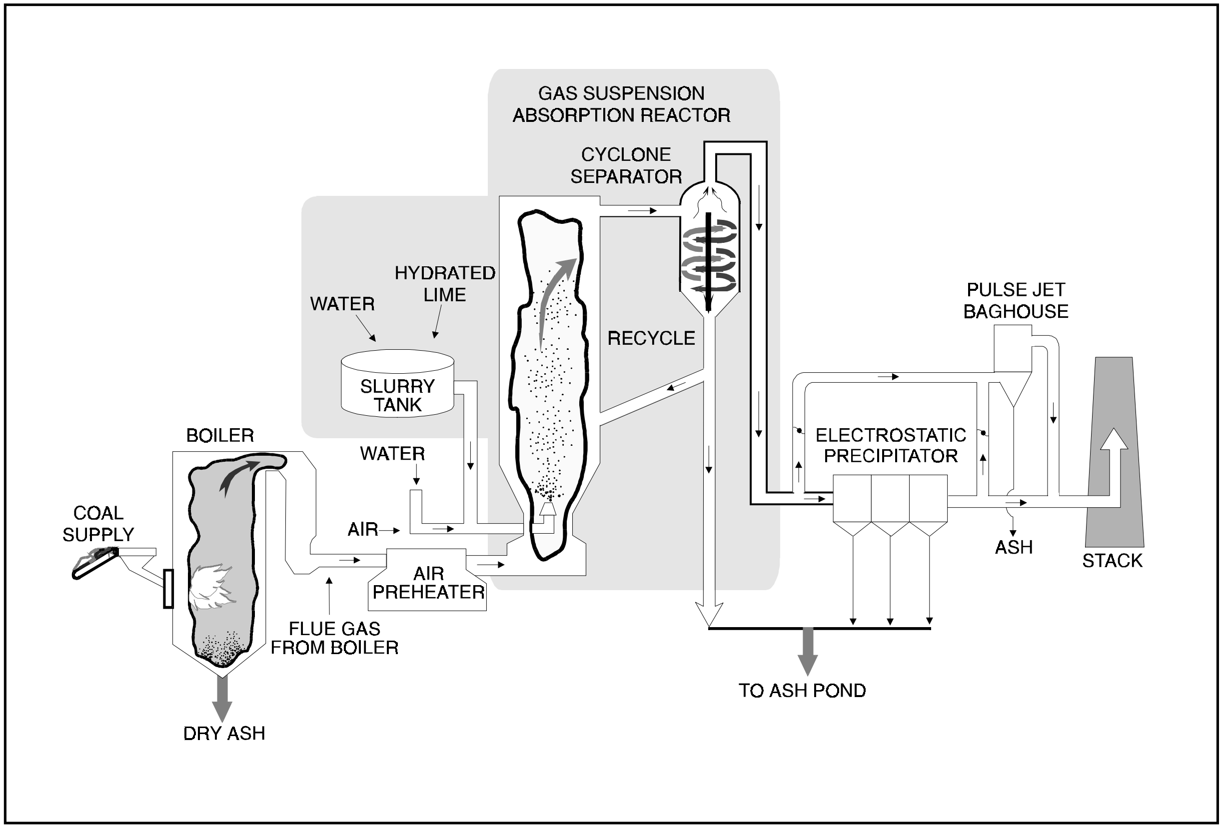
Plant Capacity/Production
10-MWe equivalent slipstream of flue gas from a 175-MWe wall-fired boiler

Coals
Western Kentucky bituminous—
Peabody Martwick, 3.05% sulfur
Emerald Energy, 2.61% sulfur
Andalax, 3.06% sulfur
Warrior Basin, 3.5% sulfur (used intermittently)

Project Funding

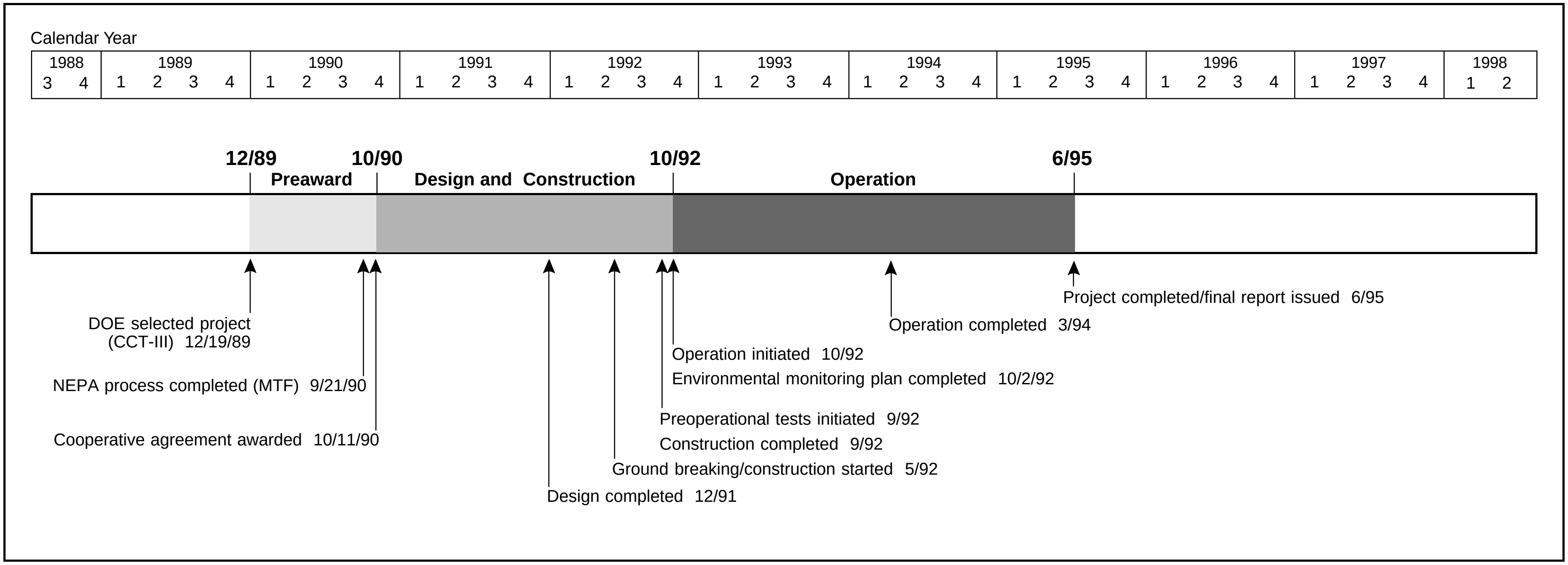
Total project cost	$7,717,189	100%
DOE	2,315,259	30
Participant	5,401,930	70

Project Objective
To demonstrate the applicability of Gas Suspension Absorption as an economic option for achieving Phase II CAAA SO_2 compliance on pulverized coal-fired boilers using high-sulfur coal.



Technology/Project Description
The GSA system consists of a vertical reactor in which flue gas comes into contact with suspended solids consisting of lime, reaction products, and fly ash. About 99% of the solids are recycled to the reactor via a cyclone while the exit gas stream passes through an electrostatic precipitator (ESP) or pulse jet baghouse (PJBH) before being released to the atmosphere. The lime slurry, prepared from hydrated lime, is injected through a spray nozzle at the bottom of the reactor. The volume of lime slurry is regulated with a variable-speed pump controlled by the measurement of the acid content in the inlet and outlet gas streams. The dilution water added to the lime slurry is controlled by on-line measurements of the flue gas exit temperature.

A test program was structured to (1) optimize design of the GSA reactor for reduction of SO_2 emissions from boilers using high-sulfur coal and (2) evaluate the environmental control capability, economic potential, and mechanical performance of GSA. A statistically designed parametric (factorial) test plan was developed involving six variables. Beyond evaluation of the basic GSA unit to control SO_2, air toxic control tests were conducted, and the effectiveness of a GSA/ESP and GSA/PJBH to control both SO_2 and particulate were tested. Factorial tests were followed by continuous runs to verify consistency of performance over time.



Results Summary

Environmental

- Ca/S molar ratio had the greatest effect on SO_2 removal, with approach-to-saturation temperature next, followed closely by chloride content.
- GSA/ESP achieved
  - 90% sulfur capture at a Ca/S molar ratio of 1.3 with 8 ºF approach-to-saturation and 0.04% chloride,
  - 90% sulfur capture at a Ca/S molar ratio of 1.4 with 18 ºF approach-to-saturation and 0.12% chloride, and
  - 99.9+% average particulate removal efficiency.
- GSA/PJBH achieved
  - 96% sulfur capture at a Ca/S molar ratio of 1.4 with 18 ºF approach-to-saturation and 0.12% chloride,
  - 3–5% increase in SO_2 reduction relative to GSA/ESP, and
  - 99.99+% average particulate removal efficiency.
- GSA/ESP and GSA/PJBH removed 98% of the hydrogen chloride (HCl), 96% of the hydrogen fluoride (HF), and 99% on more of most trace metals, except cadmium, artimony, mercury, and selenium. (GSA/PJBH removed 99+% of the selenium.)
- The solid by-product was usable as low-grade cement.

Operational

- GSA/ESP lime utilization averaged 66.1% and GSA/PJBH averaged 70.5%.
- The reactor achieved the same performance as a conventional spray dryer, but at $^1/_4$–$^1/_3$ the size.
- GSA generated lower particulate loading than a spray dryer, enabling compliance with a lower ESP efficiency.
- Special steels were not required in construction, and only a single spray nozzle is needed.
- High availability and reliability similar to other commercial applications were demonstrated, reflecting simple design.

Economic

- Capital and levelized (15-year) costs for GSA installed in a 300-MWe plant using 2.6% sulfur coal are compared below to costs for a wet limestone scrubber with forced oxidation (WLFO scrubber). EPRI's TAG™ cost method was used. Based on EPRI cost studies of FGD processes, the capital cost (1990$) for a conventional spray dryer was $172/kW.

	Capital Cost (1990 $/kW)	**Levelized Cost (mills/kWh)**
GSA—3 units at 50% capacity	149	10.35
WLFO	216	13.04

Project Summary

The GSA capability of suspending a high concentration of solids, effectively drying the solids, and recirculating the solids at a high rate with precise control results in SO_2 control comparable to that of wet scrubbers and high lime utilization. The high concentration of solids provides the sorbent/SO_2 contact area. The drying enables low approach-to-saturation temperature and chloride usage. The rapid, precise, integral recycle system sustains the high solids concentration. The high lime utilization mitigates the largest operating cost (lime) and further reduces costs by reducing the amount of by-product generated. The GSA is distinguished from the average spray dryer by its modest size, simple means of introducing reagent to the reactor, direct means of recirculating unused lime, and low reagent consumption. Also, injected slurry coats recycled solids, not the walls, avoiding corrosion and enabling use of carbon steel in fabrication.

Environmental Performance

Exhibit 5-10 lists the six variables used in the factorial tests and the levels at which they were applied. Inlet flue gas temperature was held constant at 320 ºF. Factorial testing showed that lime stoichiometry had the greatest effect on SO_2 removal. Approach-to-saturation temperature was the next most important factor, followed closely by chloride levels. Although an approach-to-saturation temperature of 8 ºF was achieved without plugging the system, the test was conducted at a very low chloride level (0.04%). Because water evaporation rates decrease as chloride levels increase, an 18 ºF approach-to-saturation temperature was chosen for the higher 0.12% coal chloride level. Exhibit 5-11 summarizes key results from factorial testing.

A 28-day continuous run to evaluate the GSA/ESP configuration was made with bituminous coals averaging 2.7% sulfur, 0.12% chloride levels, and 18 ºF approach-to-saturation temperature. A subsequent 14-day continuous run to evaluate the GSA/PJBH configuration was performed under the same conditions as those of the 28-day run, except for adjustments in flyash injection rate from 1.5–1.0 gr/ft^3 (actual).

The 28-day run on the GSA/ESP system showed that the overall SO_2 removal efficiency averaged slightly more than 90%, very close to the set point of 91%, at an average Ca/S molar ratio of 1.40–1.45 moles $Ca(OH)_2$/mole inlet SO_2. The system was able to adjust rapidly to the surge in inlet SO_2 caused by switching to 3.5% sulfur Warrior Basin coal for a week. Lime utilization averaged 66.1%. The particulate removal efficiency averaged 99.9+% and emission rates were maintained below 0.015 lb/10^6 Btu. The 14-day run on the GSA/PJBH system showed that the SO_2 removal efficiency averaged more than 96% at an average Ca/S molar ratio of 1.34–1.43 moles $Ca(OH)_2$/mole inlet SO_2. Lime utilization averaged 70.5%. The particulate removal efficiency averaged 99.99+% and emission rates ranged from 0.001–0.003 lb/10^6 Btu.

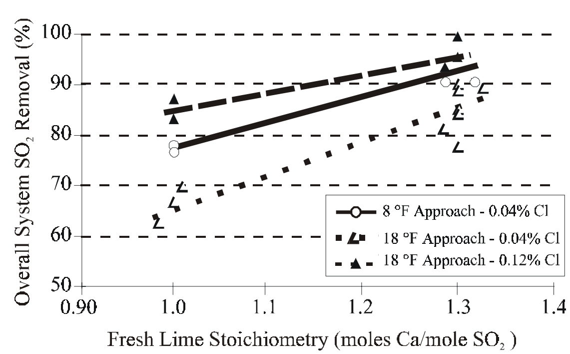
All air toxic tests were conducted with 2.7% sulfur, low-chloride coal with a 12 ºF approach-to-saturation temperature and a high flyash loading of 2.0 gr/ft^3 (actual). The GSA/ESP arrangement indicated average removal efficiencies of greater than 99% for arsenic, barium, chromium, lead, and vanadium; somewhat less for manganese; and less than 99% for antimony, cadmium, mercury, and selenium. The GSA/PJBH configuration showed 99+% removal efficiencies for arsenic, barium, chromium, lead, manganese, selenium, and vanadium; with cadmium removal much lower and mercury removal lower than that of the GSA/ESP system. The removal of HCl and HF was dependent upon the utilization of lime slurry and was relatively independent of particulate control configuration. Removal efficiencies were greater than 98% for HCl and 96% for HF.

Exhibit 5-10
Variables and Levels Used in GSA Factorial Testing

Variable	Level
Approach-to-saturation temperature (°F)	8*, 18, 28
Ca/S (moles $Ca(OH)_2$/mole inlet SO_2)	1.00 and 1.30
Flyash loading (gr/ft^3, actual)	0.50 and 2.0
Coal chloride level (%)	0.04 and 0.12
Flue gas flow rate (10^3 scfm)	14 and 20
Recycle screw speed (rpm)	30 and 45

*8 °F was only run at the low coal chloride level.

Exhibit 5-11
GSA Factorial Testing Results



Note: All tests were conducted at a 320 °F inlet flue gas temperature.

Operational Performance

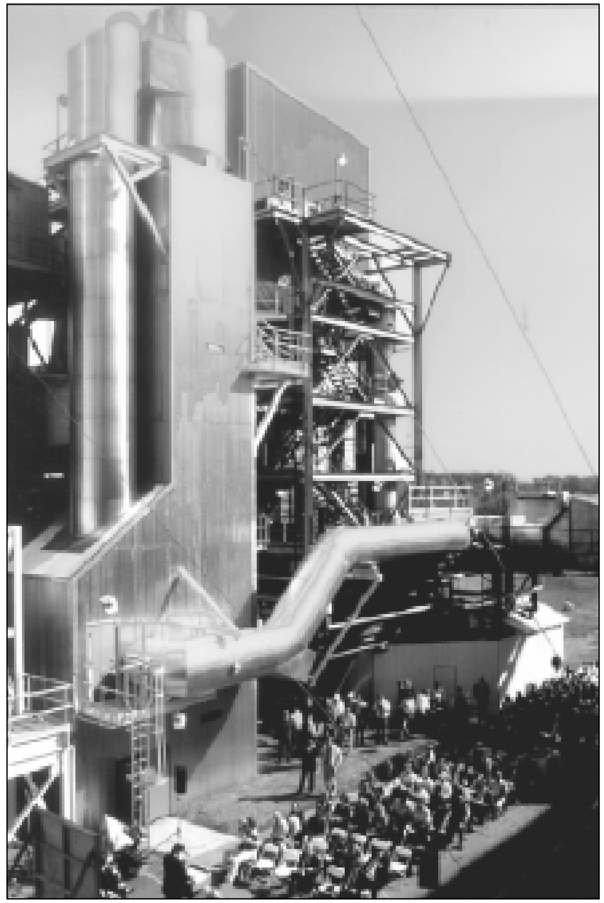
Because the GSA system has suspended recycle solids to provide a contact area for SO_2 capture, multiple high-pressure atomizer nozzles or high-speed rotary nozzles to achieve uniform, fine droplet size are not required. Also, recycle of solids is direct and avoids recycling material in the feed slurry, which necessitates expensive abrasion-resistant materials in the atomizer(s).

The high heat and mass transfer characteristics of the GSA enable the GSA system to be significantly smaller than a conventional spray dryer for the same capacity—¼ to ⅓ the size. This makes retrofit feasible for space-confined plants and reduces installation cost. The GSA system slurry is sprayed on the recycled solids, not the reactor walls, avoiding direct wall contact and the need for corrosion-resistant alloy steels. Furthermore, the high concentration of rapidly moving solids scours the reactor walls and mitigates scaling. The GSA system generates a significantly lower grain loading than a spray dryer—2–5 gr/ft^3 for GSA versus 6–10 gr/ft^3 for a spray dryer—enabling compliance even with lower ESP particulate removal efficiency. The GSA system produces a solid by-product containing very low moisture. This material contains both fly ash and unreacted lime. With the addition of water, the by-product undergoes a pozzolanic reaction, essentially providing the characteristics of a low-grade cement.

Economic Performance

Using the EPRI costing methodology applied to 30–35 other FGD processes, economics were estimated for a moderately difficult retrofit of a 300-MWe boiler burning 2.6% sulfur coal. The design SO_2 removal efficiency was 90% at a lime feed rate equivalent to 1.30 moles of Ca/mole inlet SO_2. Lime was assumed to be 2.8 times the cost of limestone. It was determined that (1) capital cost (1990$) was $149/kW with three units at 50% capacity and (2) levelized cost (15-year) was 10.35 mills/kWh with three units at 50% capacity.

A cost comparison run for a WLFO scrubber showed the capital and levelized costs to be $216/kW and 13.04 mills/kWh, respectively. The capital cost listed in EPRI cost tables for a conventional spray dryer at 300-MWe and 2.6% sulfur coal was $172/kW (1990$). Also, because the GSA requires less power and has better lime utilization than a spray dryer, the GSA will have a lower operating cost.



▲ AirPol, Inc. successfully demonstrated the GSA system at TVA's Center for Emissions Research.

Commercial Applications

The low capital cost, moderate operating cost, and high SO_2 capture efficiency make the GSA system particularly attractive as a CAAA compliance option for boilers in the 50–250-MWe range. Other major advantages include the modest space requirements comparable to duct injection systems, high availability/reliability owing to design simplicity, and low dust loading, minimizing particulate upgrade costs.

GSA market entry was significantly enhanced with the sale of a 50-MWe unit, worth $10 million, to the city of Hamilton, OH, subsidized by the Ohio Coal Development Office. A sale worth $1.3 million has been made to the U.S. Army for hazardous waste disposal. A GSA system has been sold to a Swedish iron ore sinter plant. Sales to Taiwan and India have a combined value of $5.5 million.

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References

- *10-MWe Demonstration of Gas Suspension Absorption Final Project Performance and Economics Report*. Report No. DOE/PC/90542-T9. AirPol, Inc. June 1995. (Available from NTIS as DE95016681.)
- *10-MW Demonstration of the Gas Suspension Absorption Final Public Design Report*. Report No. DOE/PC/90542-T10. AirPol, Inc. June 1995. (Available from NTIS as DE960003270.)
- *SO_2 Removal Using Gas Suspension Absorption Technology*. Topical Report No. 4. U.S. Department of Energy and AirPol, Inc. April 1995.
- 10-MWe Demonstration of the Gas Suspension Absorption Process at TVA's Center for Emissions Research: Final Report. Report No. DOE/PC/90542-T10. Tennessee Valley Authority. March 1995. (Available from NTIS as DE96000327.)

Confined Zone Dispersion Flue Gas Desulfurization Demonstration

Project completed.

Participant
Bechtel Corporation

Additional Team Members
Pennsylvania Electric Company—cofunder and host
Pennsylvania Energy Development Authority—cofunder
New York State Electric & Gas Corporation—cofunder
Rockwell Lime Company—cofunder

Location
Seward, Indiana County, PA (Pennsylvania Electric Company's Seward Station, Unit No. 5)

Technology
Bechtel Corporation's in-duct, confined zone dispersion flue gas desulfurization (CZD/FGD) process

Plant Capacity/Production
73.5-MWe equivalent

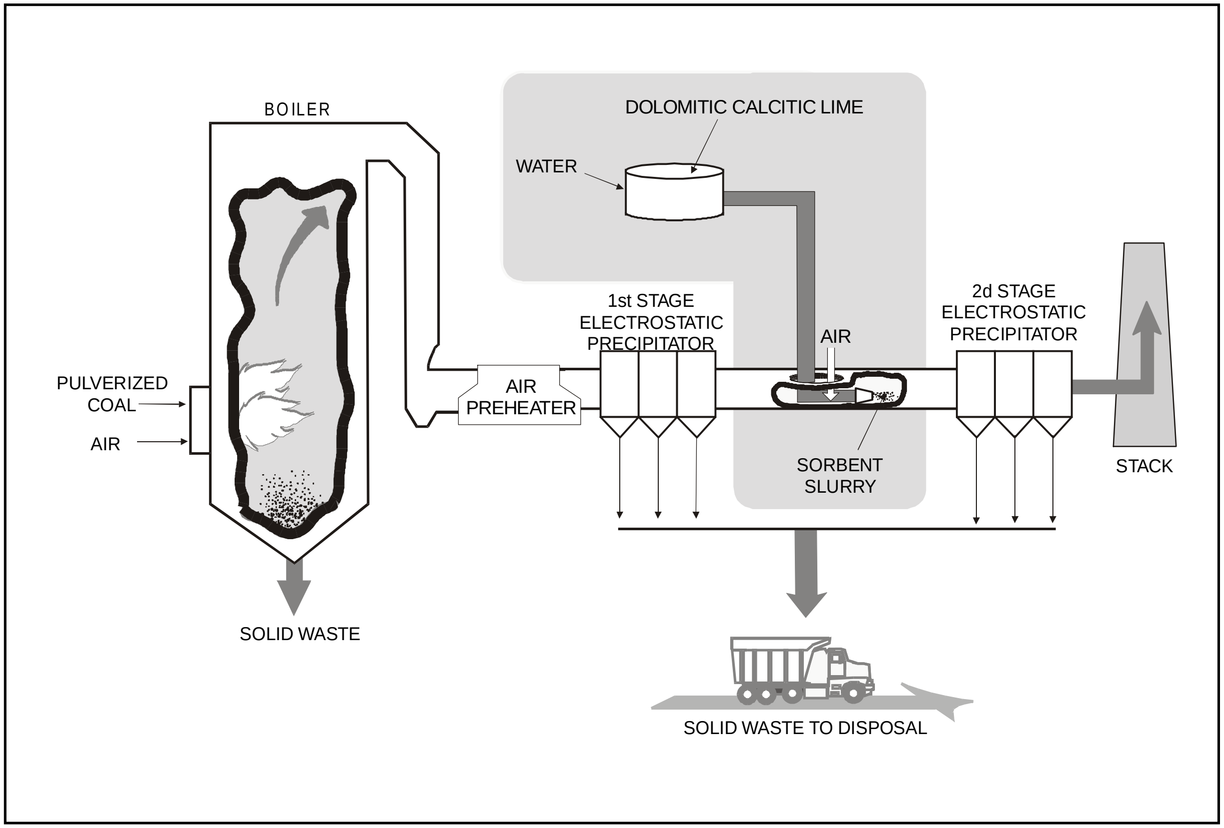
Coal
Pennsylvania bituminous, 1.2–2.5% sulfur

Project Funding

Total project cost*	$10,411,600	100%
DOE	5,205,800	50
Participant	5,205,800	50

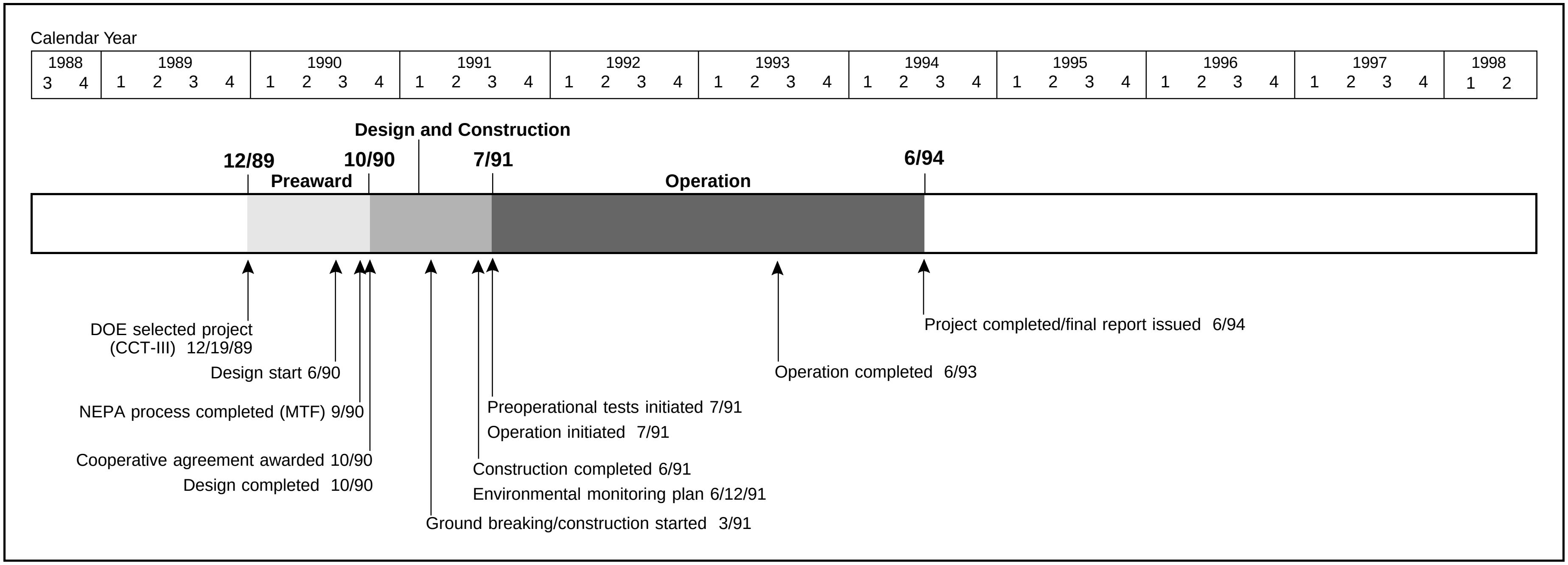
Project Objective
To demonstrate SO_2 removal capabilities of in-duct CZD/FGD technology; specifically, to define the optimum process operating parameters and to determine CZD/FGD's operability, reliability, and cost-effectiveness during long-term testing and its impact on downstream operations and emissions.

*Additional project overrun costs were funded 100% by the participant for a final total project cost of $12,173,000.



Technology/Project Description
In Bechtel's CZD/FGD process, a finely atomized slurry of reactive lime is sprayed into the flue gas stream between the boiler air heater and the electrostatic precipitator (ESP). The lime slurry is injected into the center of the duct by spray nozzles designed to produce a cone of fine spray. As the spray moves downstream and expands, the gas within the cone cools and the SO_2 is quickly absorbed in the liquid droplets. The droplets mix with the hot flue gas, and the water evaporates rapidly. Fast drying precludes wet particle buildup in the duct and aids the flue gas in carrying the dry reaction products and the unreacted lime to the ESP.

This project included injection of different types of sorbents (dolomitic and calcitic limes) with several atomizer designs using low- and high-sulfur coals to verify the effects on SO_2 removal and the capability of the ESP to control particulates. The demonstration was conducted at Pennsylvania Electric Company's Seward Station in Seward, PA. One-half of the flue gas capacity of the 147-MWe Unit No. 5 was routed through a modified, longer duct between the first- and second-stage ESPs.



Results Summary

Environmental

- Pressure-hydrated dolomitic lime proved to be a more effective sorbent than either dry hydrated calcitic lime or freshly slaked calcitic lime.
- Sorbent injection rate was the most influential parameter on SO_2 capture. Flue gas temperature was the limiting factor on injection rate. For SO_2 capture efficiency of 50% or more, a flue gas temperature of 300 ºF or more was needed.
- Slurry concentration for a given sorbent did not increase SO_2 removal efficiency beyond a certain threshold concentration.
- Testing indicated that SO_2 removal efficiencies of 50% or more were achievable with flue gas temperatures of 300–310 ºF (full load), sorbent injection rate of 52–57 gal/min, residence time of 2 seconds, and a pressure-hydrated dolomitic-lime concentration of about 9%.
- For operating conditions at Seward Station, data indicated that for 40–50% SO_2 removal, a 6–8% lime or dolomitic lime slurry concentration, and a stoichiometric ratio of 2–2.5 resulted in a 40–50% lime utilization rate. That is, 2–2.5 moles of CaO or CaO•MgO were required for every mole of SO_2 removed.
- Assuming 92% lime purity, 1.9–2.4 tons of lime was required for every ton of SO_2 removed.

Operational

- About 100 ft of straight duct was required to assure the 2-second residence time needed for effective CZD/FGD operation.
- At Seward Station, stack opacity was not detrimentally affected by CZD/FGD.
- Availability of CZD/FGD was very good.
- Some CZD/FGD modification will be necessary to assure consistent SO_2 removal and avoid deposition of solids within the ductwork during upsets.

Economic

- Capital cost of a 500-MWe system operating on 4% sulfur coal and achieving 50% SO_2 reduction was estimated at less than \$30/kW and operating cost at \$300/ton of SO_2 removed.

Project Summary

The principle of the CZD/FGD is to form a wet zone of slurry droplets in the middle of a duct confined in an envelope of hot gas between the wet zone and the hot gas. The lime slurry reacts with part of the SO_2 in the gas and the reaction products dry to form solid particles. An ESP, downstream from the point of injection, captures the reaction products along with the fly ash entrained in the flue gas.

CZD/FGD did not require a special reactor, simply a modification to the ductwork. Use of the commercially available Type S pressure-hydrated dolomitic lime reduced residence time requirements for CZD/FGD and enhanced sorbent utilization. The increased humidity of CZD/FGD processed flue gas enhanced ESP performance, eliminating the need for upgrades to handle the increased particulate load.

Bechtel began its 18-month, two-part test program for the CZD process in July 1991, with the first 12 months of the test program consisting primarily of parametric testing and the last 6 months consisting of continuous operational testing. During the continuous operational test period, the system was operated under fully automatic control by the host utility boiler operators. The new atomizing nozzles were thoroughly tested both outside and inside the duct prior to testing. The SO_2 removal parametric test program, which began in October 1991, was completed in August 1992.

Specific objectives were as follows:

- Achieve projected SO_2 removal of 50%
- Realize SO_2 removal costs of less than $300/ton
- Eliminate negative effects on normal boiler operations without increasing particulate emissions and opacity

The parametric tests included duct injection of atomized lime slurry made of dry hydrated calcitic lime, freshly slaked calcitic lime, and pressure-hydrated dolomitic lime. All three reagents remove SO_2 from the flue gas but require different feed concentrations of lime slurry for the same percentage of SO_2 removed. The most efficient removals and easiest to operate system were obtained using pressure-hydrated dolomitic lime.

▲ Bechtel's demonstration showed that 50% SO_2 removal efficiency was possible using CZD/FGD technology. The extended duct into which lime slurry was injected is in the foreground.

Environmental Performance

Sorbent injection rate proved to be the most influential factor on SO_2 capture. The rate of injection possible was limited by the flue gas temperature. This impacted a portion of the demonstration when air leakage caused flue gas temperature to drop from 300–310 ºF to 260–280 ºF. At 300–310 ºF, injection rates of 52–57 gal/min were possible and SO_2 reductions greater than 50% were achieved. At 260–280 ºF, injection rates had to be dropped to 30–40 gal/min, resulting in a 15–30% drop in SO_2 removal efficiency. Slurry concentration for a given sorbent did not increase SO_2 removal efficiency beyond a certain threshold concentration. For example, with pressure-hydrated dolomitic lime, slurry concentrations above 9% did not increase SO_2 capture efficiency.

Parametric tests indicated that SO_2 removals above 50% are possible under the following conditions: flue gas temperature of 300–310 ºF; boiler load of 145–147-MWe; residence time in the duct of 2 seconds; and lime slurry injection rate of 52–57 gal/min.

Operational Performance

The percentage of lime utilization in the CZD/FGD significantly affected the total cost of SO_2 removal. An analysis of the continuous operational data indicated that the percentage of lime utilization was directly dependent on two key factors:

- Percentage of SO_2 removed
- Lime slurry feed concentration

For operating conditions at Seward Station, data indicated that for 40–50% SO_2 removal, a 6–8% lime or dolomitic lime slurry concentration, and a stoichiometric ratio of 2–2.5 resulted in a 40–50% lime utilization rate. That is, 2–2.5 moles of CaO or CaO•MgO were required for every mole of SO_2 removed; or assuming 92% lime purity, 1.9–2.4 tons of lime were required for every ton of SO_2 removed. In summary, the demonstration showed the following results:

- A 50% SO_2 removal efficiency with CZD/FGD was possible.
- Drying and SO_2 absorption required a residence time of 2 seconds, which required a long and straight horizontal gas duct of about 100 feet.
- The fully automated system integrated with the power plant operation demonstrated that the CZD/FGD process responded well to automated control operation. However, modifications to the CZD/FGD were required to assure consistent SO_2 removal and avoid deposition of solids within the gas duct during upsets.
- Availability of the system was very good.
- At Seward Station, stack opacity was not detrimentally affected by the CZD/FGD system.

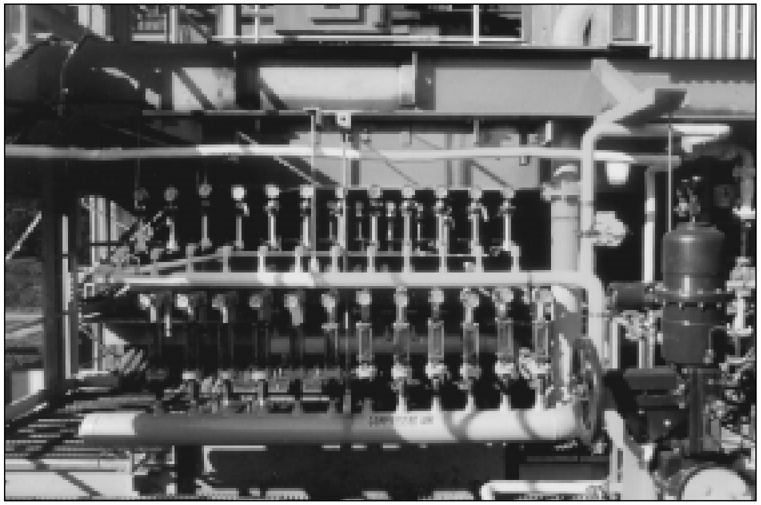
Economic Performance

The CZD/FGD process can achieve costs of \$300/ton of SO_2 removed when operating a 500-MWe unit burning 4% sulfur coal. Based on a 500-MWe plant retrofitted with CZD/FGD for 50% SO_2 removal, the total capital cost is estimated to be less than \$30/kW.

Commercial Applications

After the conclusion of the DOE-funded CZD/FGD demonstration project at Seward Station, the CZD/FGD system was modified to improve SO_2 removal during continuous operation while following daily load cycles. Bechtel and the host utility, Pennsylvania Electric Company, continued the CZD/FGD demonstration for an additional year. Results showed that CZD/FGD operation at SO_2 removal rates lower than 50% could be sustained over long periods without significant process problems.

CZD/FGD can be used for retrofit of existing plants and installation in new utility boiler flue gas facilities to remove SO_2 from a wide variety of sulfur-containing coals. A CZD/FGD system can be added to a utility boiler with a capital investment of about \$25–50/kW of installed capacity, or approximately one-fourth the cost of building a conventional wet scrubber. In addition to low capital cost, other advantages include small space requirements, ease of retrofit, low energy requirements, fully automated operation, and production of only nontoxic, disposable waste. The CZD/FGD technology is particularly well suited for retrofitting existing boilers, independent of type, age, or size. The CZD/FGD installation does not require major power station alterations and can be easily and economically integrated into existing power plants.



▲ This photo shows the CZD/FGD lime slurry injector control system.

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References

- *Confined Zone Dispersion Project: Final Technical Report*. Bechtel Corporation. June 1994.
- *Confined Zone Dispersion Project: Public Design Report.* Bechtel Corporation. October 1993.
- *Comprehensive Report to Congress on the Clean Coal Technology Program: Confined Zone Dispersion Flue Gas Desulfurization Demonstration.* Bechtel Corporation. Report No. DOE/FE-0203P. U.S. Department of Energy. September 1990. (Available from NTIS as DE91002564.)

LIFAC Sorbent Injection Desulfurization Demonstration Project

Project completed.

Participant

LIFAC–North America (a joint venture partnership between Tampella Power Corporation and ICF Kaiser Engineers, Inc.)

Additional Team Members

ICF Kaiser Engineers, Inc.—cofunder and project manager
Tampella Power Corporation—cofunder
Tampella, Ltd.—technology owner
Richmond Power and Light—cofunder and host utility
Electric Power Research Institute—cofunder
Black Beauty Coal Company—cofunder
State of Indiana—cofunder

Location

Richmond, Wayne County, IN (Richmond Power & Light's Whitewater Valley Station, Unit No. 2)

Technology

LIFAC's sorbent injection process with sulfur capture in a unique, patented vertical activation reactor

Plant Capacity/Production

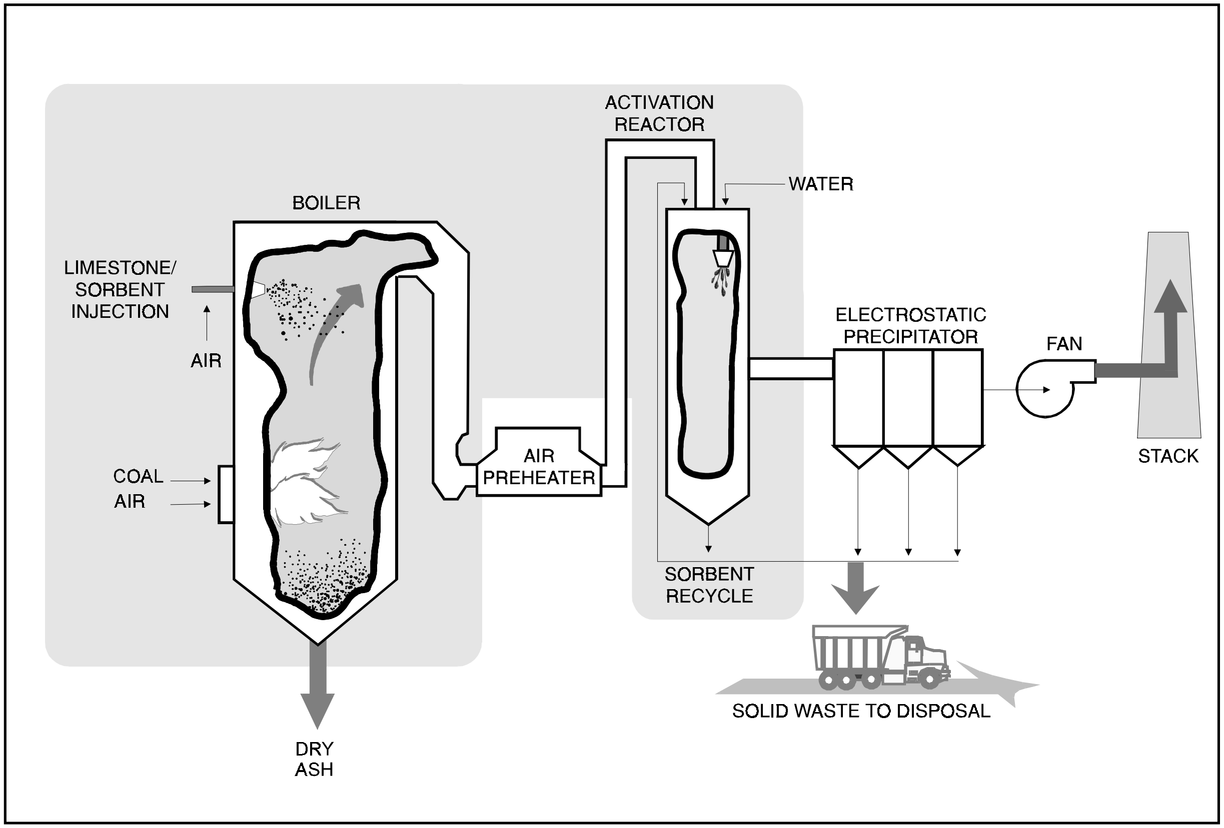
60-MWe

Coal

Bituminous, 2.0–2.8% sulfur

Project Funding

Total project cost	$21,393,772	100%
DOE	10,636,864	50
Participants	10,756,908	50



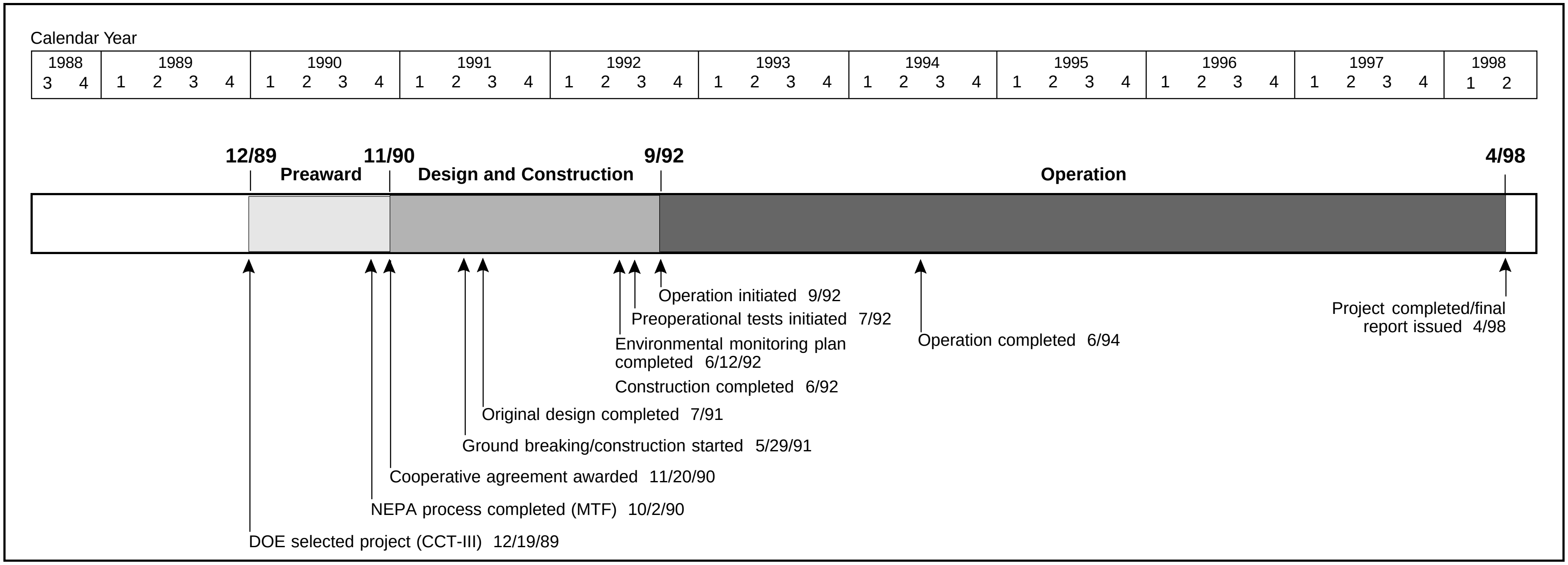
Project Objective

To demonstrate that electric power plants—especially those with space limitations and burning high-sulfur coals—can be retrofitted successfully with the LIFAC limestone injection process to remove 75–85% of the SO_2 from flue gas and produce a dry solid waste product for disposal in a landfill.

Technology/Project Description

Pulverized limestone is pneumatically blown into the upper part of the boiler near the superheater where it absorbs some of the SO_2 in the boiler flue gas. The limestone is calcined into calcium oxide and is available for capture of additional SO_2 downstream in the activation, or humidification, reactor. In the vertical chamber, water sprays initiate a series of chemical reactions leading to SO_2 capture. After leaving the chamber, the sorbent is easily separated from the flue gas along with the fly ash in the electrostatic precipitator (ESP). The sorbent material from the reactor and electrostatic precipitator are recirculated back through the reactor for increased efficiency. The waste is dry, making it easier to handle than the wet scrubber sludge produced by conventional wet limestone scrubber systems.

The technology enables power plants with space limitations to use high-sulfur midwestern coals by providing an injection process that removes 75–85% of the SO_2 from flue gas and produces a dry solid waste product suitable for disposal in a landfill.



Results Summary

Environmental

- SO_2 removal efficiency was 70% at a calcium-to-sulfur (Ca/S) molar ratio of 2.0, approach-to-saturation temperature of 7–12 ºF, and limestone fineness of 80% minus 325 mesh.
- SO_2 removal efficiency with limestone fineness of 80% minus 200 mesh was 15% lower at a Ca/S molar ratio of 2.0 and 7–12 ºF approach to saturation.
- The four parameters having the greatest influence on sulfur removal efficiency were limestone quality, Ca/S molar ratio, approach-to-saturation temperature, and ESP ash recycle rate.
- ESP ash recycle rate was limited in the demonstration system configuration. Increasing the recycle rate and sustaining a 5 ºF approach-to-saturation temperature was projected to increase SO_2 removal efficiency to 85% at a Ca/S molar ratio of 2.0 (fine limestone).
- ESP efficiency and operating levels were essentially unaffected by LIFAC operation during steady-state operation.
- Fly and bottom ash were dry and readily disposed of at a local landfill. The quantity of additional solid waste can be determined by assuming that approximately 4.3 tons of limestone is required to remove 1.0 ton of SO_2.

Operational

- When operating with fine limestone (80% minus 325 mesh), the soot-blowing cycle had to be reduced from 6.0 to 4.5 hours.
- Automated programmable logic and simple design make the LIFAC system easy to operate in start-up, shutdown, or normal duty cycles.
- The amount of bottom ash increased slightly, but there was no negative impact on the ash-handling system.

Economic

- Capital cost—$66/kW for two LIFAC reactors (300-MWe); $76/kW for one LIFAC reactor (150-MWe); $99/kW for one LIFAC reactor (65-MWe).
- Operating cost—$65/ton of SO_2 removal, assuming 75% SO_2 capture, Ca/S molar ratio of 2.0, limestone composed of 95% $CaCO_3$, and $15/ton.

Project Summary

The LIFAC technology was designed to enhance the effectiveness of dry sorbent injection systems for SO_2 control and to maintain the desirable aspects of low capital cost and compactness for ease of retrofit. Furthermore, limestone was used as the sorbent (about 1/3 of the cost of lime) and a sorbent recycle system was incorporated to reduce operating costs.

The process evaluation test plan was composed of five distinct phases each having its own objectives. These tests were as follows:

- Baseline tests characterized the operation of the host boiler and associated subsystems prior to LIFAC operations.
- Parametric tests were designed to evaluate the many possible combinations of LIFAC process parameters and their effect on SO_2 removal.
- Optimization tests were performed after the parametric tests to evaluate the reliability and operability of the LIFAC process over short, continuous operating periods.
- Long-term tests were performed to demonstrate LIFAC's performance under commercial operating conditions.
- Post-LIFAC tests involved repeating the baseline test to identify any changes caused by the LIFAC system.

The coals used during the demonstration varied in sulfur content from 1.4–2.8%. However, most of the testing was conducted with the higher sulfur coals (2.0–2.8% sulfur).

Environmental Performance

During the parametric testing phase, the numerous LIFAC process values and their effects on sulfur removal efficiency were evaluated. The four major parameters having the greatest influence on sulfur removal efficiency were limestone quality, Ca/S molar ratio, reactor bottom temperature (approach-to-saturation), and ESP ash recycling rate. Total SO_2 capture was about 15% better when injecting fine limestone (80% minus 325 mesh) than it was with coarse limestone (80% minus 200 mesh).

While injecting the fine limestone, the soot blowing frequency had to be increased from 6-hour to 4.5-hour cycle periods. The coarse-quality limestone did not affect soot blowing but was found to be more abrasive on the feed and transport hoses.

Parametric tests indicated that a 70% SO_2 reduction was achievable with a Ca/S molar ratio of 2.0. ESP ash containing unspent sorbent and fly ash was recycled from the ESP hoppers back into the reactor inlet duct work. Ash recycling is essential for efficient SO_2 capture. The large quantity of ash removed from the LIFAC reactor bottom and the small size of the ESP hoppers limited the ESP ash recycling rate. As a result, the amount of material recycled from the ESP was approximately 70% less than had been anticipated. However, this low recycling rate was found to affect SO_2 capture. During a brief test, it was found that increasing the recycle rate by 50% resulted in a 5% increase in SO_2 removal efficiency. It was estimated that if the reactor bottom ash is recycled along with ESP ash, while sustaining a reactor temperature of 5 ºF above saturation temperature, an SO_2 reduction of 85% could be maintained.

Operational Performance

Optimization testing began in March 1994 and was followed by long-term testing in June 1994. The boiler was operated at an average load of 60-MWe during long-term testing, although it fluctuated according to power demand. The LIFAC process automatically adjusted to boiler load changes. A Ca/S molar ratio of 2.0 was selected to attain SO_2 reductions above 70%. Reactor bottom temperature was about 5 ºF higher than optimum to avoid ash buildup on the steam reheaters. Atomized water droplet size was smaller than optimum for the same reason. Other key process parameters held constant during the long-term tests included the degree of humidification, grind size of the high-calcium-content limestone, and recycle of spent sorbent from the ESP.

Long-term testing showed that SO_2 reductions of 70% or more can be maintained under normal boiler operating ranges. Stack opacity was low (about 10%) and ESP efficiency was high (99.2%). The amount of boiler bottom ash increased slightly during testing, but there was no negative impact on the power plant's bottom and flyash removal system. The solid waste generated was a mixture of fly ash and calcium compounds and was readily disposed of at a local landfill.

▲ The LIFAC system successfully demonstrated at Whitewater Valley Station Unit No. 2 is being retained by Richmond Power & Light for commercial use with high-sulfur coal. There are 10 full-scale LIFAC units in Canada, China, Finland, Russia, and the United States.

The LIFAC system proved to be highly operable because it has few moving parts and is simple to operate. The process can be easily shut down and restarted. The process is automated by a programmable logic system, which regulates process control loops, interlocking, start-up, shutdowns, and data collection. The entire LIFAC process was easily managed via two personal computers located in the host utility's control room.

▲ The top of the LIFAC reactor is shown being lifted into place. During 2,800 hours of operation, long-term testing showed that SO_2 reductions of 70% or more could be sustained under normal boiler operation.

Economic Performance

The economic evaluation indicated that the capital cost of a LIFAC installation is lower than for either a spray dryer or wet scrubber. Capital costs for LIFAC technology vary, depending on unit size and the quantity of reactors needed:

- $99/kW for one LIFAC reactor at Whitewater Valley Station (65-MWe)
- $76/kW for one LIFAC reactor at Shand Station (150-MWe)
- $66/kW for two LIFAC reactors at Shand Station (300-MWe)

Crushed limestone accounts for about one half of LIFAC's operating costs. LIFAC requires 4.3 tons of limestone to remove 1.0 ton of SO_2, assuming 75% SO_2 capture, a Ca/S molar ratio of 2.0, and limestone containing 95% $CaCO_3$. Assuming limestone costs of $15/ton, LIFAC's operating cost would be $65/ton of SO_2 removed.

Commercial Applications

There are 10 full-scale LIFAC units in operation in Canada, China, Finland, Russia, and the United States. The LIFAC system at Richmond Power & Light is the first to be applied to a power plant using high-sulfur (2.0–2.9%) coal. The LIFAC system is being retained by Richmond Power & Light at Whitewater Valley Station, Unit No. 2. The other LIFAC installations on power plants are using bituminous and lignite coals having lower sulfur contents (0.6–1.5%).

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References

- *LIFAC Sorbent Injection Desulfurization Demonstration Project. Final Report, Vol. II: Project Performance and Economics.* LIFAC–North America. February 1998. (Available from NTIS as DE96004421.)
- "LIFAC Nearing Marketability." *Clean Coal Today.* Report No. DOE/FE-0215P-21. Spring 1996.
- Viiala, J., et al. "Commercialization of the LIFAC Sorbent Injection Process in North America." *Third Annual Clean Coal Technology Conference: Technical Papers.* September 1994.
- *Comprehensive Report to Congress on the Clean Coal Technology Program: LIFAC Sorbent Injection Desulfurization Demonstration Project.* LIFAC–North America. Report No. DOE/FE-0207P. U.S. Department of Energy, October 1990. (Available from NTIS as DE91001077.)

Advanced Flue Gas Desulfurization Demonstration Project

Project completed.

Participant

Pure Air on the Lake, L.P. (a project company of Pure Air, which is a general partnership between Air Products and Chemicals, Inc., and Mitsubishi Heavy Industries America, Inc.)

Additional Team Members

Northern Indiana Public Service Company—cofunder and host
Mitsubishi Heavy Industries, Ltd.—process designer
United Engineers and Constructors (Stearns-Roger Division)—facility designer
Air Products and Chemicals, Inc.—constructor and operator

Location

Chesterton, Porter County, IN (Northern Indiana Public Service Company's Bailly Generating Station, Unit Nos. 7 and 8)

Technology

Pure Air's advanced flue gas desulfurization (AFGD) process

Plant Capacity/Production

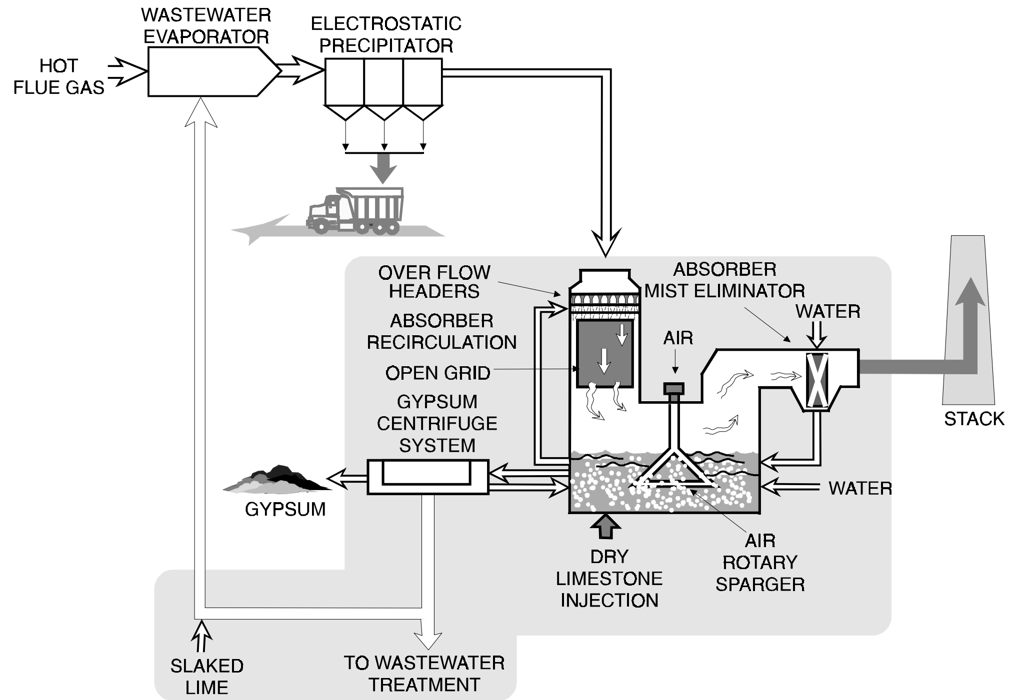
528-MWe

Coal

Bituminous, 2.0–4.5% sulfur

Project Funding

Total project cost	$151,707,898	100%
DOE	63,913,200	42
Participant	87,794,698	58



Project Objective

To reduce SO_2 emissions by 95% or more at approximately one-half the cost of conventional scrubbing technology, significantly reduce space requirements, and create no new waste streams.

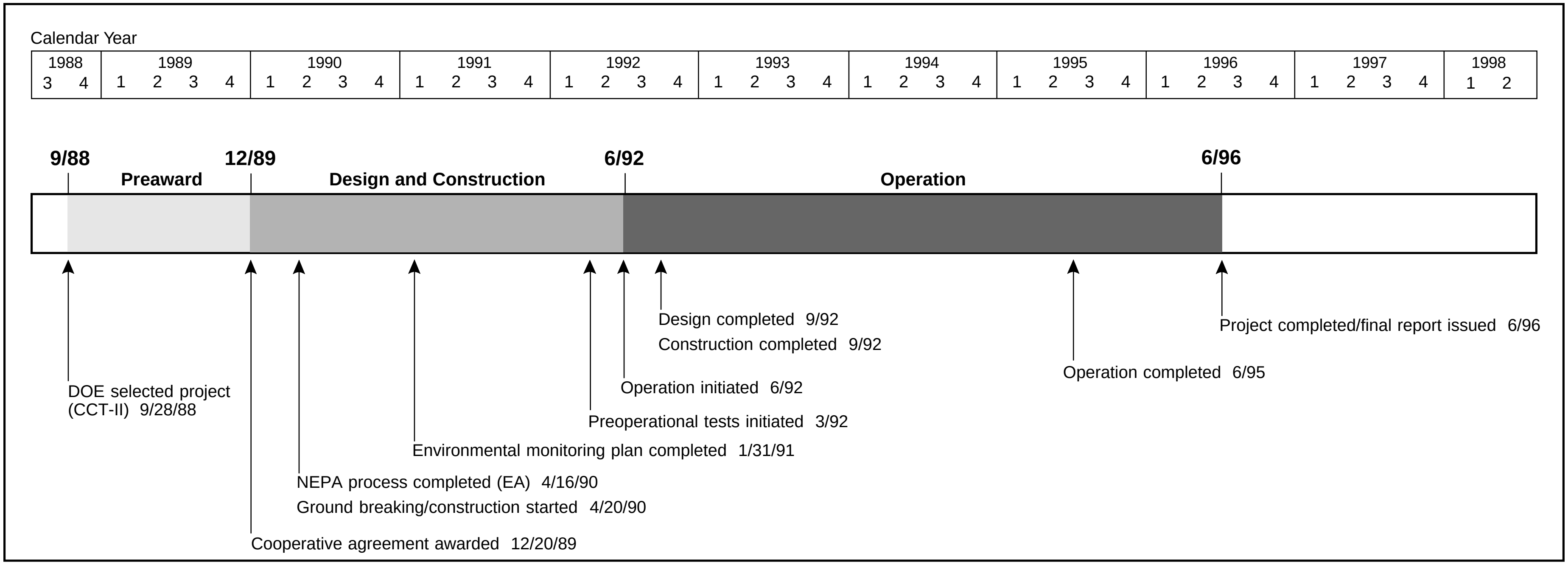
Technology/Project Description

Pure Air built a single SO_2 absorber for a 528-MWe power plant. Although the largest capacity absorber module of its time in the United States, space requirements were modest because no spare or backup absorber modules were required. The absorber performed three functions in a single vessel: prequenching, absorbering, and oxidation of sludge to gypsum. Additionally, the absorber was of a co-current design, in which the flue gas and scrubbing slurry move in the same direction and at a relatively high velocity compared to that in conventional scrubbers. These features all combined to yield a state-of-the-art SO_2 absorber that was more compact and less expensive than contemporary conventional scrubbers.

Other technical features included the injection of pulverized limestone directly into the absorber, a device called an air rotary sparger located within the base of the absorber, and a novel wastewater evaporation system. The air rotary sparger combined the functions of agitation and air distribution into one piece of equipment to facilitate the oxidation of calcium sulfite to gypsum.

Pure Air also demonstrated a unique gypsum agglomeration process, PowerChip®, to significantly enhance handling characteristics of adsorbed flue gas desulfurization (AFGD)-derived gypsum.

PowerChip is a registered trademark of Pure Air on the Lake, L.P.



Results Summary

Environmental

- AFGD design enabled a single 600-MWe absorber module without spares to remove 95% or more SO_2 at availabilities of 99.5% when operating with high-sulfur coals.
- Wallboard-grade gypsum was produced in lieu of solid waste, and all gypsum produced was sold commercially.
- The wastewater evaporation system (WES) mitigated expected increases in wastewater generation associated with gypsum production and showed the potential for achieving zero wastewater discharge (only a partial-capacity WES was installed).
- PowerChip® increased the market potential for AFGD-derived gypsum by cost effectively converting it to a product with the handling characteristics of natural rock gypsum.
- Air toxics testing established that all acid gases were effectively captured and neutralized by the AFGD. Trace elements largely became constituents of the solids streams (bottom ash, fly ash, gypsum product). Some boron, selenium, and mercury passed to the stack gas in a vapor state.

Operational

- AFGD use of co-current, high-velocity flow; integration of functions; and a unique air rotary sparger proved to be highly efficient, reliable (to the exclusion of requiring a spare module), and compact. The compactness, combined with no need for a spare module, significantly reduced space requirements.
- The own-and-operate contractual arrangement whereby Pure Air took on the turnkey, financing, operating and maintenance risks through performance guarantees was successful.

Economic

- Capital costs and space requirements for AFGD were about half those of contemporary systems.

Project Summary

The project proved that single absorber modules of advanced design could process large volumes of flue gas and provide the required availability and reliability without the usual spares. The major performance objectives were met.

Over the 3-year demonstration, the AFGD unit accumulated 26,280 hours of operation with an availability of 99.5%. Approximately 237,000 tons of SO_2 were removed, with capture efficiencies of 95% or more, and over 210,000 tons of salable gypsum were produced. The AFGD continues commercial service, which includes sale of all by-product gypsum to U.S. Gypsum's East Chicago, IN, wallboard production plant.

Environmental Performance

Testing over the 3-year period clearly established that AFGD operating within its design parameters (without additives) could consistently achieve 95% SO_2 reduction or more with 2.0–4.5% sulfur coals. The design range for the calcium-to-sulfur stoichiometric ratio was 1.01–

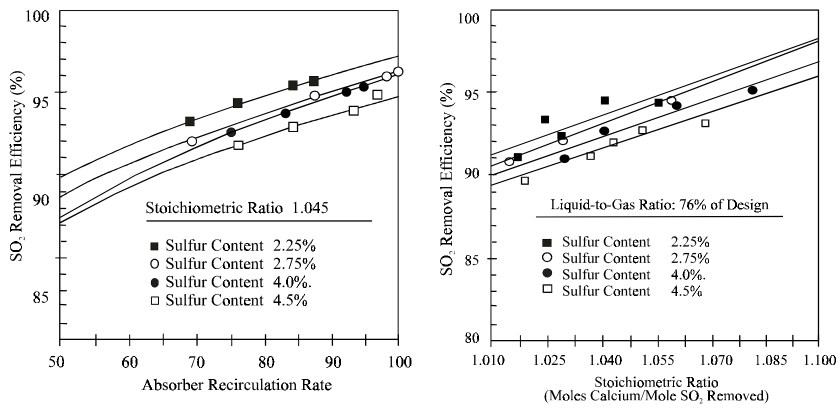
1.07, with the upper value set by gypsum purity requirements (i.e., amount of unreacted reagent allowed in the gypsum). Another key control parameter was the ratio L/G, which is the amount of reagent slurry injected into the absorber grid (L) to the volume of flue gas (G). The design L/G range was 50–128 gal/10^3 ft^3. The lower end was determined by solids settling rates in the slurry and the requirement for full wetting of the grid packing. The high end was determined by where performance leveled out.

Five coals with differing sulfur contents were selected for parametric testing to examine SO_2 removal efficiency as a function of load, sulfur content, stoichiometric ratio, and L/G. Loads tested were 33%, 67%, and 100%. High removal efficiencies, well above 95%, at loads of 33% and 67% were possible with low to moderate stoichiometric ratio and L/G settings, even for 4.5% sulfur coal. Exhibit 5-12 summarizes the results of parametric testing at full load.

In the AFGD process, chlorides that would have been released to the air are captured and potentially become a wastewater problem. This was mitigated by the addition of the WES which takes a portion of the wastewater stream with high chloride and sulfate levels and injects it into the ductwork upstream of the ESP. The hot flue gas evaporated the water and the dissolved solids were captured in the ESP. Problems were experienced early on, with the WES nozzles failing to provide adequate atomization and plugging as well. This was resolved by replacing the original single-fluid nozzles with dual fluid systems employing air as the second fluid.

Commercial-grade gypsum quality (95.6–99.7%) was maintained throughout testing, even at the lower sulfur concentrations where the ratio of fly ash to gypsum increases due to lower sulfate availability. The primary importance of producing a commercial-grade gypsum is avoidance of the environmental and economic consequences of disposal. The marketability of the gypsum is dependent upon whether users are in range of economic transport and whether they can handle the gypsum by-product. For these reasons, PowerChip® technology was demonstrated as part of the project. This technology uses a compression mill to convert the highly cohesive AFGD gypsum cake into a flaked product with handling characteristics equivalent to natural rock gypsum. The process avoids use of binders, pre-drying or pre-calcining normally associated with briquetting and is 30–55% cheaper at $2.50–$4.10/ton.

Exhibit 5-12
SO_2 Removal Performance
(100% Boiler Load)



Air toxics testing established that all acid gases are effectively captured and neutralized by the AFGD. Trace elements largely become constituents of the solids streams (bottom ash, fly ash, gypsum product). Some boron, selenium, and mercury pass to the stack gas in a vapor state.

Operational Performance

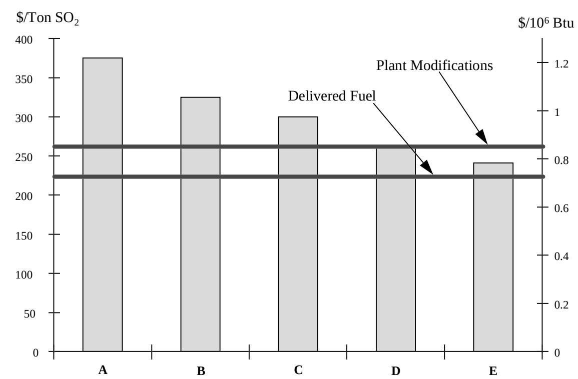
Availability over the 3-year operating period averaged 99.5% while maintaining an average SO_2 removal efficiency of 94%. This was attributable to the simple, effective design and an effective operating/maintenance philosophy. Modifications were also made to the AFGD system. An example was the implementation of new alloy technology, C-276 alloy over carbon steel clad material, to replace alloy wallpaper construction within the absorber tower wet/dry interface. Also, use of co-current rather than conventional counter-current flow resulted in lower pressure drops across the absorber and afforded the flexibility to increase gas flow without an abrupt drop in removal efficiency. AFGD SO_2 capture efficiency with limestone was comparable to that in wet scrubbers using lime, which is far more expensive. Twenty-four-hour power consumption was 5,275 kW, or 61% of expected consumption, and water consumption was 1,560 gal/min, or 52% of expected consumption.

Economic Performance

Exhibit 5-13 summarizes capital and levelized current dollar cost estimates for nine cases with varying plant capacity and coal sulfur content. A capacity factor of 65% and a sulfur removal efficiency of 90% were assumed. The calculation of levelized cost followed guidelines established in the Electric Power Research Institute's Technical Assessment Guide.

The incremental benefits of the own-and-operate arrangement, by-product utilization, and emission allowances were also evaluated. Exhibit 5-14 depicts the relative costs of a hypothetical 500-MWe generating unit in the Midwest burning 4.3% sulfur coal with a base case conventional FGD system and four incremental cases.

Exhibit 5-14
Flue Gas Desulfurization Economics



500-MWe plant, 30-yr levelized costs, allowance value of $300/ton

Incremental cases:

A—Conventional FGD (EPRI model)

B—AFGD, own-and-operate arrangement

C—Adds gypsum sales

D—Adds emission allowance credits at $300/ton, for 90% SO_2 removal

The horizontal lines in Exhibit 5-15 show the range of costs for a fuel-switching option. The lower bar is the cost of fuel delivered to the hypothetical midwest unit and the upper bar allows for some plant modifications to accommodate the compliance fuel.

Commercial Applications

AFGD is positioned well to compete in the pollution control arena of 2000 and beyond. AFGD has markedly reduced cost and demonstrated the ability to compete with fuel switching under certain circumstances even with a first-generation system. Advances in technology, e.g., in materials and components, should improve costs for AFGD. The own-and-operate business approach has done much to mitigate risk on the part of prospective users.

High SO_2-capture efficiency places an AFGD user in the possible position of trading allowances or applying credits to other units within the utility. WES and PowerChip® mitigate or eliminate otherwise serious environmental concerns. AFGD effectively deals with hazardous air pollutants.

The project received *Power* magazine's 1993 Powerplant Award and the National Society of Professional Engineer's 1992 Outstanding Engineering Achievement Award.

Contacts

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James U. Watts, FETC, (412) 892-5991

References

- *Advanced Flue Gas Desulfurization (AFGD) Demonstration Project. Final Technical Report, Vol. II: Project Performance and Economics.* Pure Air on the Lake, L.P. April 1996. (Available from NTIS as DE96050313.)
- *Advanced Flue Gas Desulfurization Project: Public Design Report.* Pure Air on the Lake, L.P. March 1990.
- *Comprehensive Report to Congress on the Clean Coal Technology Program: Advanced Flue Gas Desulfurization (AFGD) Demonstration Project.* (Pure Air on the Lake, L.P.) DOE/FE Report No. 0150. U.S. Department of Energy. November 1989. (Available from NTIS as DE90004460.)
- *Summary of Air Toxics Emissions Testing at Sixteen Utility Power Plants.* Prepared by Burns and Roe Services Corporation for U.S. Department of Energy, Pittsburgh Energy Technology Center. July 1996.

Exhibit 5-13
Estimated Costs for an AFGD System
(1995 Current Dollars)

Cases:	1	2	3	4	5	6	7	8	9
Plant size (MWe)	100	100	100	300	300	300	500	500	500
Coal sulfur content (%)	1.5	3.0	4.5	1.5	3.0	4.5	1.5	3.0	4.5
Capital cost ($/kW)	193	210	227	111	121	131	86	94	101
Levelized cost ($/ton SO_2)									
15-year life	1,518	840	603	720	401	294	536	302	223
20-year life	1,527	846	607	716	399	294	531	300	223
Levelized cost (mills/kWh)									
15-year life	16.39	18.15	19.55	7.78	8.65	9.54	5.79	6.52	7.24
20-year life	16.49	18.28	19.68	7.73	8.62	9.52	5.74	6.48	7.21

Demonstration of Innovative Applications of Technology for the CT-121 FGD Process

Project completed.

Participant

Southern Company Services, Inc.

Additional Team Members

Georgia Power Company—host
Electric Power Research Institute—cofunder
Radian Corporation—environmental and analytical consultant
Ershigs, Inc.—fiberglass fabricator
Composite Construction and Equipment—fiberglass sustainment consultant
Acentech—flow modeling consultant
Ardaman—gypsum stacking consultant
University of Georgia Research Foundation—by-product utilization studies consultant

Location

Newnan, Coweta County, GA (Georgia Power Company's Plant Yates, Unit No. 1)

Technology

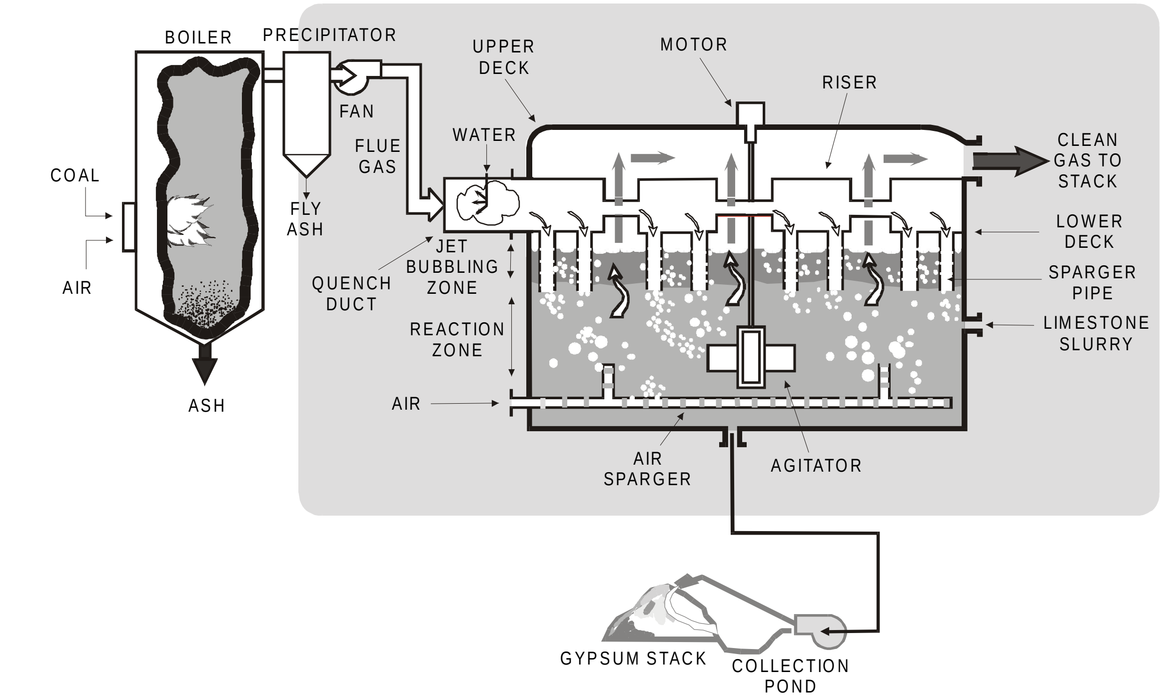
Chiyoda Corporation's Chiyoda Thoroughbred-121 (CT-121) advanced flue gas desulfurization (FGD) process

Plant Capacity/Production

100-MWe

Coals

Illinois No. 5 & No. 6 blend, 2.4% sulfur
Compliance, 1.2% sulfur



Project Funding

Total project cost	$43,074,996	100%
DOE	21,085,211	49
Participant	21,989,785	51

Project Objective

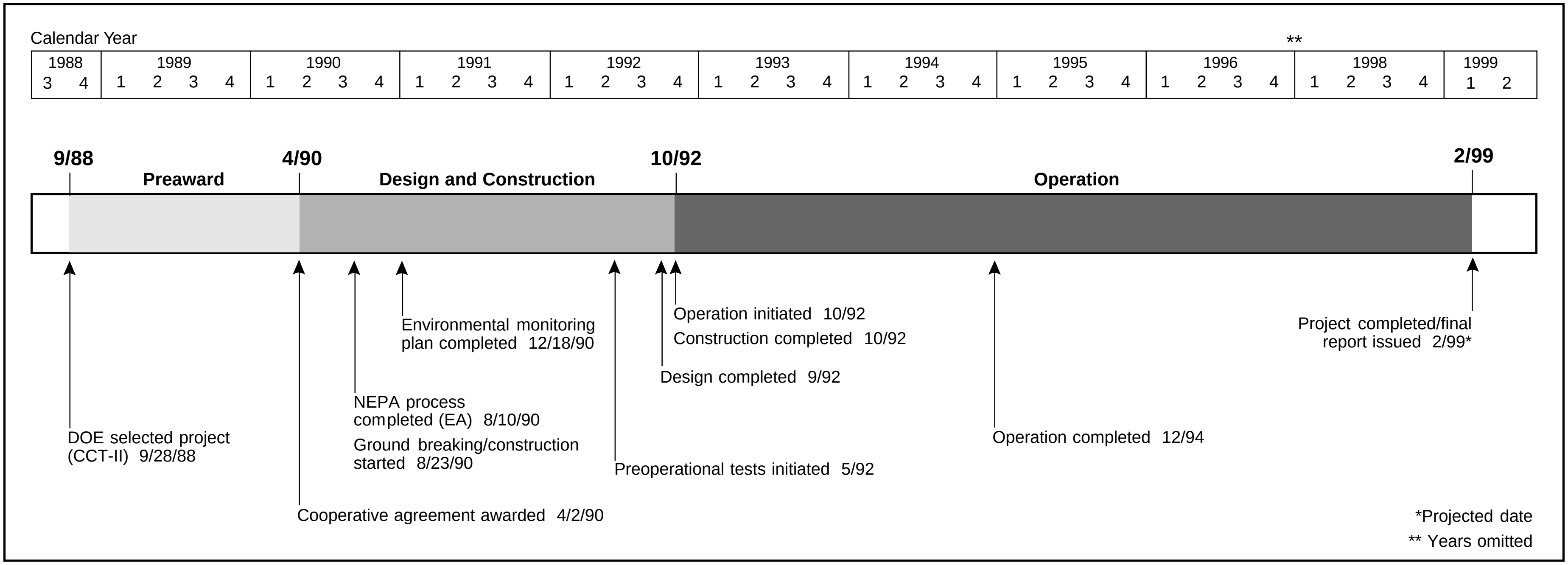
To demonstrate 90% SO_2 control at high reliability with and without simultaneous particulate control; to evaluate use of fiberglass-reinforced-plastic (FRP) vessels to eliminate flue gas reheat and spare absorber modules; and to evaluate use of gypsum to reduce waste management costs.

Technology/Project Description

The project demonstrated the CT-121 FGD process, which uses a unique absorber design known as the Jet Bubbling Reactor® (JBR). The process combines limestone FGD reaction, forced oxidation, and gypsum crystallization in one process vessel. The process is mechanically and chemically simpler than conventional FGD processes and can be expected to exhibit lower cost characteristics.

The flue gas enters underneath the scrubbing solution in the Jet Bubbling Reactor®. The SO_2 in the flue gas is absorbed and forms calcium sulfite ($CaSO_3$). Air is bubbled into the bottom of the solution to oxidize the calcium sulfite to form gypsum. The slurry is dewatered in a gypsum stack, which involves filling a dyked area with gypsum slurry. Gypsum solids settle in the dyked area by gravity, and clear water flows to a retention pond. The clear water from the pond is returned to the process.

Jet Bubbling Reactor is a registered trademark of the Chiyoda



Results Summary

Environmental

- Over 90% SO_2 removal efficiency was achieved at SO_2 inlet concentrations of 1,000–3,500 ppm with limestone utilization over 97%.
- JBR achieved particulate removal efficiencies of 97.7–99.3% for inlet mass loadings of 0.303–1.392 lb/10^6 Btu over a load range of 50–100-MWe.
- Capture efficiency was a function of particle size:
  - >10 microns—99% capture
  - 1–10 microns—90% capture
  - 0.5–1 micron—negligible capture
  - <0.5 micron—90% capture
- Hazardous air pollutant (HAP) testing showed greater than 95% capture of hydrogen chloride (HCl) and fluoride (HF) gases, 80–98% capture of most trace metals, less than 50% capture of mercury and cadmium, and less than 70% capture of selenium.
- Gypsum stacking proved effective for producing wallboard/cement-grade gypsum.

Operational

- FRP-fabricated equipment proved durable both structurally and chemically, eliminating the need for a flue gas prescrubber and reheat.
- FRP construction combined with simplicity of design resulted in 97% availability at low ash loadings and 95% at high ash loadings, precluding the need for a spare reactor module.
- Simultaneous SO_2 and particulate control were achieved at flyash loadings reflective of an ESP with marginal performance.

Economic

- Final results are not yet available. However, elimination of the need for flue gas prescrubbing, reheat, and spare module requirement should result in capital requirements far below those of conventional FGD systems.

Project Summary

The CT-121 process differs from the more common spray tower type of flue gas desulfurization systems in that a single process vessel is used in place of the usual spray tower/reaction tank/thickener arrangement. Pumping of reacted slurry to a gypsum transfer tank is intermittent. This allows crystal growth to proceed essentially uninterrupted resulting in large, easily dewatered gypsum crystals (conventional systems employ large centrifugal pumps to move reacted slurry causing crystal attrition and secondary nucleation).

The demonstration spanned 27 months, including start-up and shakedown, during which approximately 19,000 hours were logged. Exhibit 5-15 summarizes operating statistics. Elevated particulate loading included a short test with the electrostatic precipitator (ESP) completely deenergized, but the long-term testing was conducted with the ESP partially deenergized to simulate a more realistic scenario, i.e., a CT-121 retrofit to a boiler with a marginally performing particulate collection device. The SO_2 removal efficiency was measured under five different inlet concentrations with coals averaging 2.4% and ranging 1.2– 4.3% sulfur (as burned).

Operating Performance

Use of FRP construction proved very successful. Because their large size precluded shipment, the JBR and limestone slurry storage tanks were constructed on site. Except for some erosion experienced at the JBR inlet transition duct, the FRP-fabricated equipment proved to be durable both structurally and chemically. Because of the high corrosion resistance, the need for a flue gas prescrubber to remove chlorides was eliminated. Similarly, the FRP-constructed chimney proved resistant to the corrosive condensates in wet flue gas, precluding the need for flue gas reheat.

Availability of the CT-121 scrubber during the low-ash test phase was 97%. It dropped to 95% under the elevated ash-loading conditions due largely to sparger tube plugging problems precipitated by flyash agglomeration on the sparger tube walls during high ash loading when the ESP was deenergized. The high reliability demonstrated verified that a spare JBR is not required in a commercial design offering.

Environmental Performance

Exhibit 5-16 shows SO_2 removal efficiency as a function of pressure drop across the JBR for five different inlet concentrations. The greater the pressure drop, the greater the depth of slurry traversed by the flue gas. As the SO_2 concentration increased, removal efficiency decreased, but adjustments in JBR fluid level could maintain the efficiency above 90% and, at lower SO_2 concentration levels, above 98%. Limestone utilization remained above 97% throughout the demonstration.

Long-term particulate capture performance was tested with a partially deenergized ESP (approximately 90% efficiency) and is summarized in Exhibit 5-17.

Analysis indicated that a large percentage of the outlet particulate matter is sulfate, likely a result of acid mist and gypsum carryover. This reduces the estimate of ash mass loading at the outlet to approximately 70% of the measured outlet particulates.

Exhibit 5-16
SO_2 Removal Efficiency

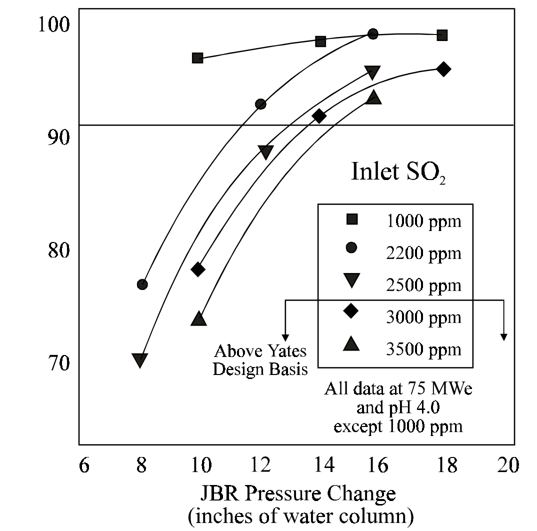


Exhibit 5-15
Operation of CT-121 Scrubber

	Low-Ash Phase	Elevated-Ash Phase	Cumulative for Project
Total test period (hr)	11,750	7,250	19,000
Scrubber available (hr)	11,430	6,310	18,340
Scrubber operating (hr)	8,600	5,210	13,810
Scrubber called upon (hr)	8,800	5,490	14,290
Reliability[a]	0.98	0.95	0.96
Availability[b]	0.97	0.95	0.97
Utilization[c]	0.73	0.72	0.75

[a] Reliability = hours scrubber operated divided by the hours called upon to operate
[b] Availability = hours scrubber available divided by the total hours in the period
[c] Utilization = hours scrubber operated divided by the total hours in the period

Exhibit 5-17
Particulate Capture Performance
(ESP Marginally Operating)

JBR Pressure Change (inches of water column)	Boiler Load (MWe)	Inlet Mass Loading ($lb/10^6$ Btu)	Outlet Mass Loading* ($lb/10^6$ Btu)	Removal Efficiency (%)
18	100	1.288	0.02	97.7
10	100	1.392	0.010	99.3
18	50	0.325	0.005	98.5
10	50	0.303	0.006	98.0

*Federal NSPS is 0.03 $lb/10^6$ Btu for units constructed after September 18, 1978. Plant Yates permit limit is 0.24 $lb/10^6$ Btu as an existing unit.

For particulate sizes greater than 10 microns, capture efficiency was consistently greater than 99%. In the 1–10-micron range, capture efficiency was over 90%. Between 0.5 and 1 micron, the particulate removal dropped at times to negligible values possibly due to acid mist carry-over entraining particulates in this size range. Below 0.5 micron, the capture efficiency increased to over 90%. Calculated HAP removals across the CT-121 JBR, based on the measurements taken during the demonstration, are shown in Exhibit 5-18.

As to solids handling, the gypsum stacking method proved effective in the long term. Although chloride content was initially high in the stack due to the closed loop nature of the process (with concentrations often exceeding 35,000 ppm), a year later the chloride concentration in the gypsum dropped to less than 50 ppm, suitable for wallboard and cement applications. The predominant cause of the initial high chloride content was attributed to rainwater washing the stack.

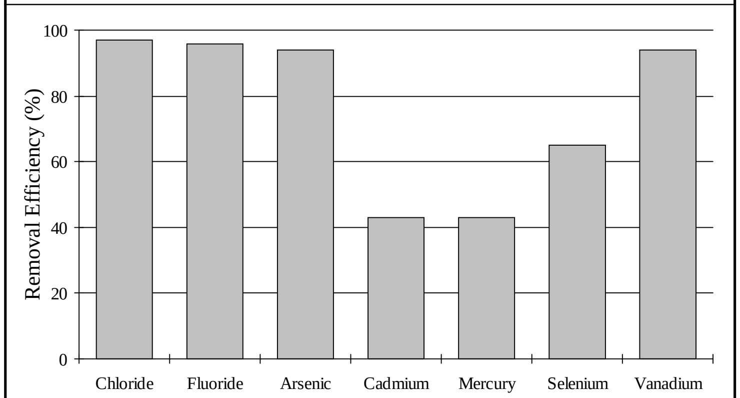
Economic Performance

Although the final economic analyses are not yet available, it appears as though CT-121 technology offers significant economic advantages. FRP construction eliminates the need for prescrubbing and reheating flue gas. High system availability eliminates the need for a spare absorber module. Particulate removal capability precludes the need for expensive (capital-intensive) ESP upgrades to meet increasingly tough environmental regulations.

Commercial Applications

Involvement of Southern Company (which owns Southern Company Services, Inc.), with more than 20,000-MWe of coal-fired generating capacity, is expected to enhance confidence in the CT-121 process among other large high-sulfur-coal boiler users. This process will be applicable to 370,000-MWe of new and existing generating capacity by the year 2010. A 90% reduction in SO_2 emissions from only the retrofit portion of this capacity represents more than 10,500,000 tons/yr of potential SO_2 control.

Exhibit 5-18
CT-121 Air Toxics Removal
(JBR Components Only)



▲ The unique Jet Bubbling Reactor® (center) was constructed from fiberglass-reinforced plastic.

Plant Yates continues to operate with the CT-121 scrubber as an integral part of the site's CAAA compliance strategy. Since the CCT Program demonstration, over 8,200 MWe equivalent of CT-121 FGD Capacity has been sold to 16 customers in seven countries.

The project received *Power* magazine's 1994 Powerplant Award. Other awards include the Society of Plastics Industries' 1995 Design Award for the mist eliminator, the Georgia Chapter of the Air and Waste Management Association's 1994 Outstanding Achievement Award, and the Georgia Chamber of Commerce's 1993 Environmental Award.

Contacts

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James U. Watts, DOE/FETC, (412) 892-5991

References

- *A Study of Toxic Emissions from a Coal-Fired Power Plant Utilizing an ESP while Demonstrating the CCT CT-121 FGD Project. Final Report.* Report No. DOE/PC/93253-T1. Radian Corporation. June 1994. (Available from NTIS as DE94016053.)
- *Comprehensive Report to Congress on the Clean Coal Technology Program: Demonstration of Innovative Applications of Technology for the CT-121 FGD Process.* Southern Company Services, Inc. Report No. DOE/FE-0158. U.S. Department of Energy. February 1990. (Available from NTIS as DE9008110.)

Environmental Control Devices
NO_x Control Technology

Micronized Coal Reburning Demonstration for NO_x Control

Participant

New York State Electric & Gas Corporation

Additional Team Members

Eastman Kodak Company—host and cofunder
Consolidation Coal Company— tester
D.B. Riley—technology supplier
Fuller Company—technology supplier
Energy and Environmental Research Corporation—reburn system designer
New York State Energy Research and Development Authority—cofunder
Empire State Electric Energy Research Corporation—cofunder

Locations

Lansing, Tompkins County, NY (New York State Electric & Gas Corporation's Milliken Station, Unit No. 1)
Rochester, Monroe County, NY (Eastman Kodak Company's Kodak Park Site Power Plant, Unit No. 15)

Technology

D.B. Riley's MPS mill (at Milliken Station)
Fuller's MicroMill™ technologies for producing micronized coal (at Eastman Kodak)

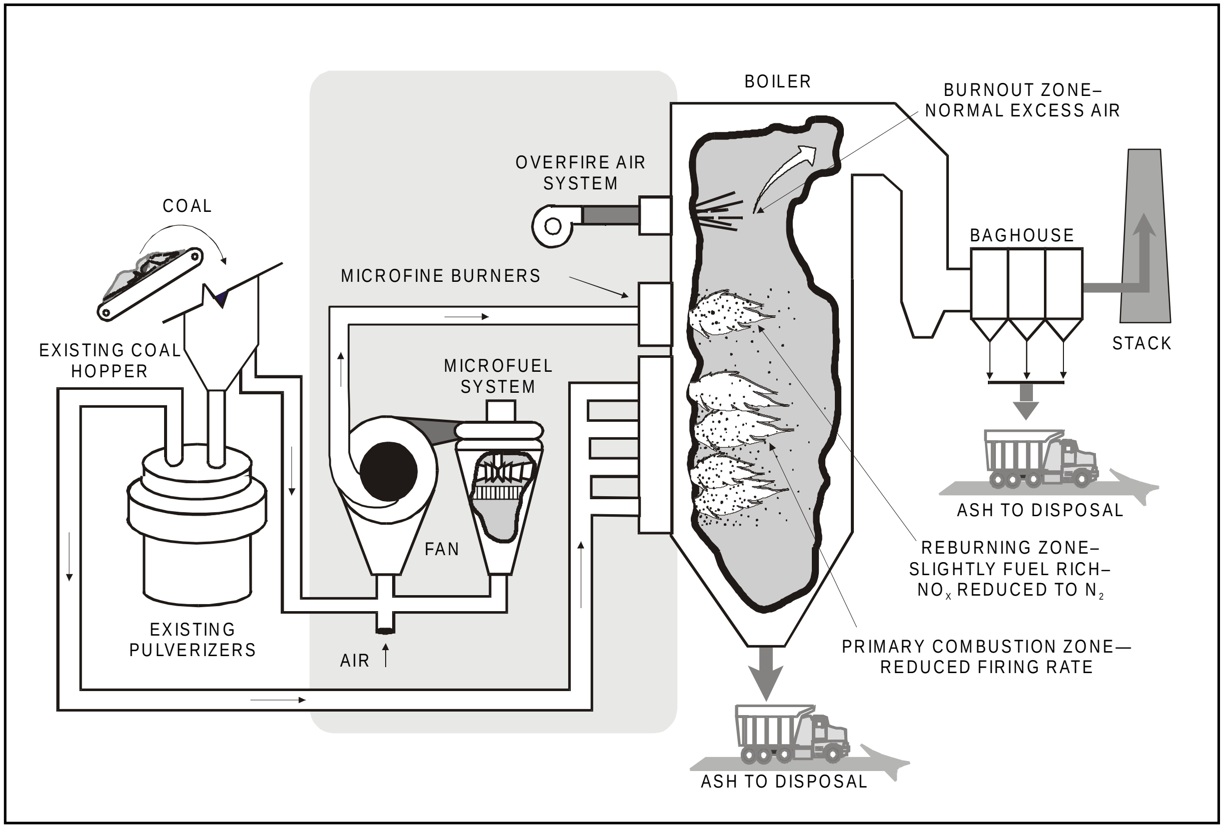
Plant Capacity/Production

Milliken Station: 148-MWe tangentially fired boiler
Eastman Kodak Company: 50-MWe cyclone boiler

Project Funding

Total project cost	$9,096,486	100%
DOE	2,701,011	30
Participant	6,395,475	70

MicroMill is a trademark of the Fuller Company.
LNCFS is a trademark of ABB Combustion Engineering, Inc.



Project Objective

To reduce NO_x emissions by 50–60% using micronized coal as the reburning fuel combined with advanced coal-reburning technology.

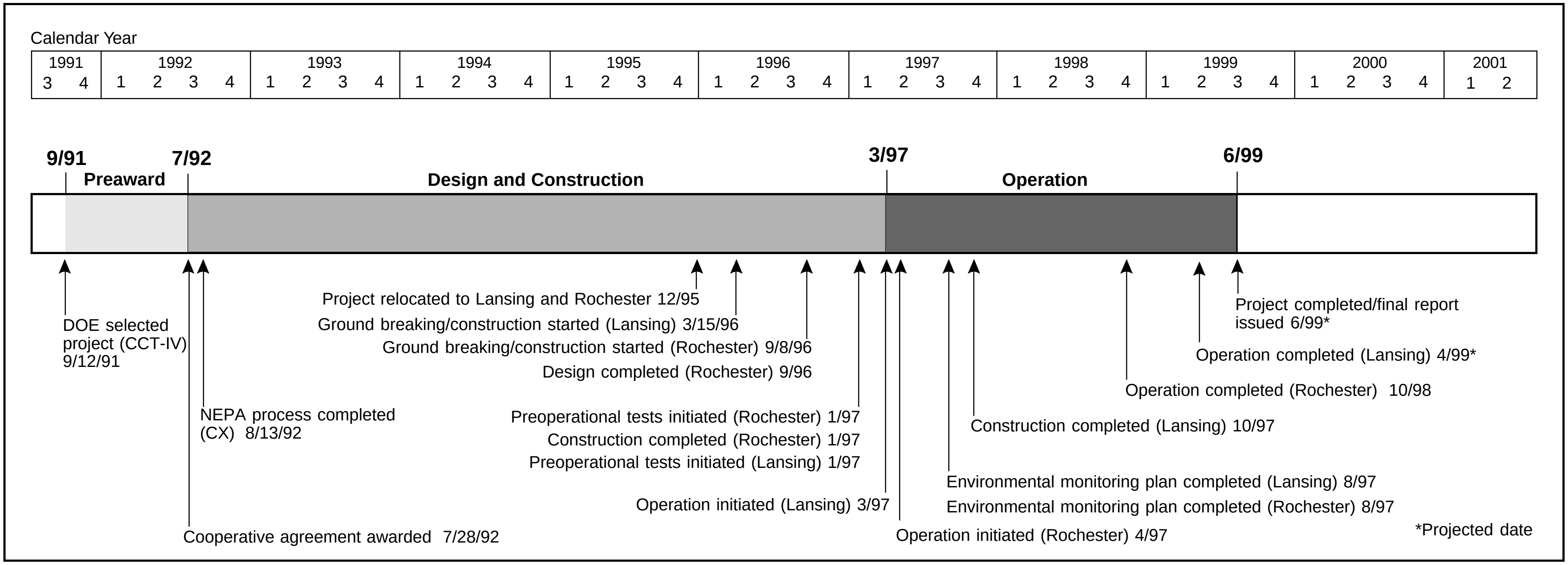
Technology/Project Description

The reburning coal, which can comprise up to 30% of the total fuel, is micronized (80% below 325 mesh) and injected into a pulverized-coal-fired furnace above the main burner, the region where NO_x formation occurs.

Micronized coal has the surface area and combustion characteristics of an atomized oil flame, which allows carbon conversion within milliseconds and release of volatiles at a more even rate. This uniform, compact combustion envelope allows for complete combustion of the coal/air mixture in a smaller furnace volume than conventional pulverized coal because heat rate, carbon loss, boiler efficiency, and NO_x formation are affected by coal fineness.

The combination of micronized coal, supplying 20% of the total furnace fuel requirements, and advanced reburning, in conjunction with fuel/air staging, provides flexible options for significant combustion operations and environmental improvements. These options can prevent higher operating costs or furnace performance derating often associated with conventional environmental controls.

At the Milliken site, coal will be reburned for NO_x control using the following methods: (1) close-coupled overfire air (CCOFA) reburning in which the top burner of the LNCFS III™ burners are used for burning the micronized coal and the remaining burners are re-aimed and (2) use of the burners in a deep stage combustion



mode and re-aiming them to create primary combustion and reburn zones. At the Eastman Kodak site, the Fuller MicroMill™ is used to produce the micronized coal, and injectors or burners, depending on boiler characteristics, will be used for the reburning. Overfire air also will be installed.

Project Status/Accomplishments

Parametric testing at the Kodak site is complete. Tests showed that the target NO_x emission level of 0.60 lb/10^6 Btu could be met with a reburn fuel heat input as low as 18.5%, representing a 56% reduction from baseline emissions. Long-term testing at optimum conditions established in the parametric tests is complete. The project is now focused on system and component reliability.

Parametric testing at the Milliken site is finished as well. The primary objective was to determine conditions that will achieve minimum NO_x emissions without exceeding 4.5% loss-on-ignition (LOI) to maintain marketability of the fly ash. Burner tilt, reburn fuel fineness, reburn fuel flow rate, and primary air flow showed little impact on NO_x emissions, but significant impact on LOI. Only excess air had a significant impact on both NO_x emissions and LOI. Ongoing tests are exploring optimum conditions for sustained NO_x control at low LOI.

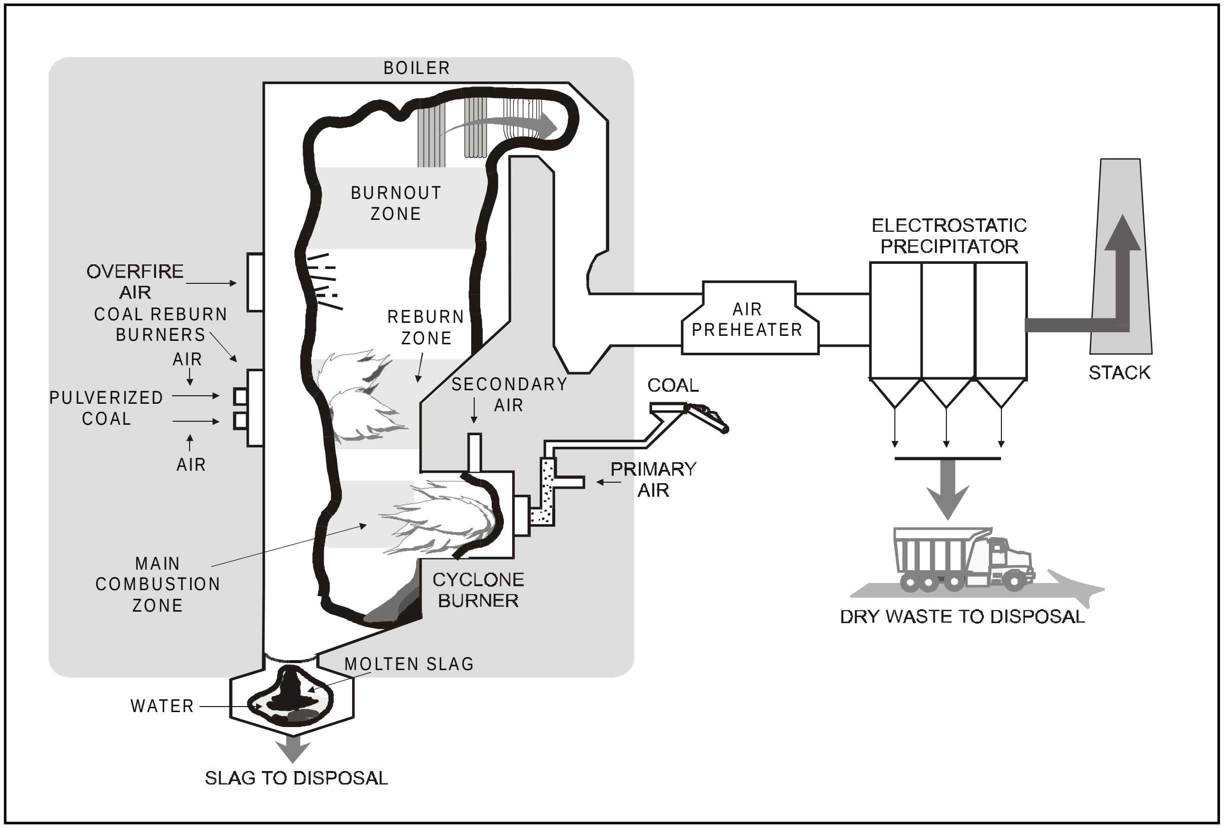
Commercial Applications

Micronized-coal-reburning technology can be applied to existing and greenfield cyclone-fired, wall-fired, and tangential-fired pulverized coal units. The technology reduces NO_x emissions by 50–60% with minimal furnace modifications for existing units. About 25% of the more than 1,000 existing units could benefit from use of this technology.

The availability of a coal-reburning fuel, as an additional fuel to the furnace, solves several problems concurrently. Existing units unable to switch fuels because of limited mill and burner capacity would be able to reach their maximum continuous rating. NO_x emissions reductions will enable lost capacity to be restored, creating a very economic source of generation. For both retrofit and greenfield facilities, reburn burners also can serve as low-load burners, and commercial units can achieve a turndown of 8:1 on nights and weekends without consuming expensive auxiliary fuel. Existing pulverizers can be operated on a variety of coals with improved performance. The combination of micronized-coal-reburning fuel and better pulverizer performance will increase overall pulverized-fuel surface area for better carbon burnout.

Demonstration of Coal Reburning for Cyclone Boiler NO_x Control

Project completed.



Participant
The Babcock & Wilcox Company

Additional Team Members
Wisconsin Power and Light Company—cofunder and host
Sargent and Lundy—engineer for coal handler
Electric Power Research Institute—cofunder
State of Illinois, Department of Energy and Natural Resources—cofunder
Utility companies (14 cyclone boiler operators)—cofunders

Location
Cassville, Grant County, WI (Wisconsin Power and Light Company's Nelson Dewey Station, Unit No. 2)

Technology
The Babcock & Wilcox Company's coal-reburning system, Coal Reburn

Plant Capacity/Production
100-MWe

Coals
Illinois Basin bituminous (Lamar), 1.15% sulfur, 1.24% nitrogen
Powder River Basin (PRB) subbituminous, 0.27% sulfur, 0.55% nitrogen

Project Funding

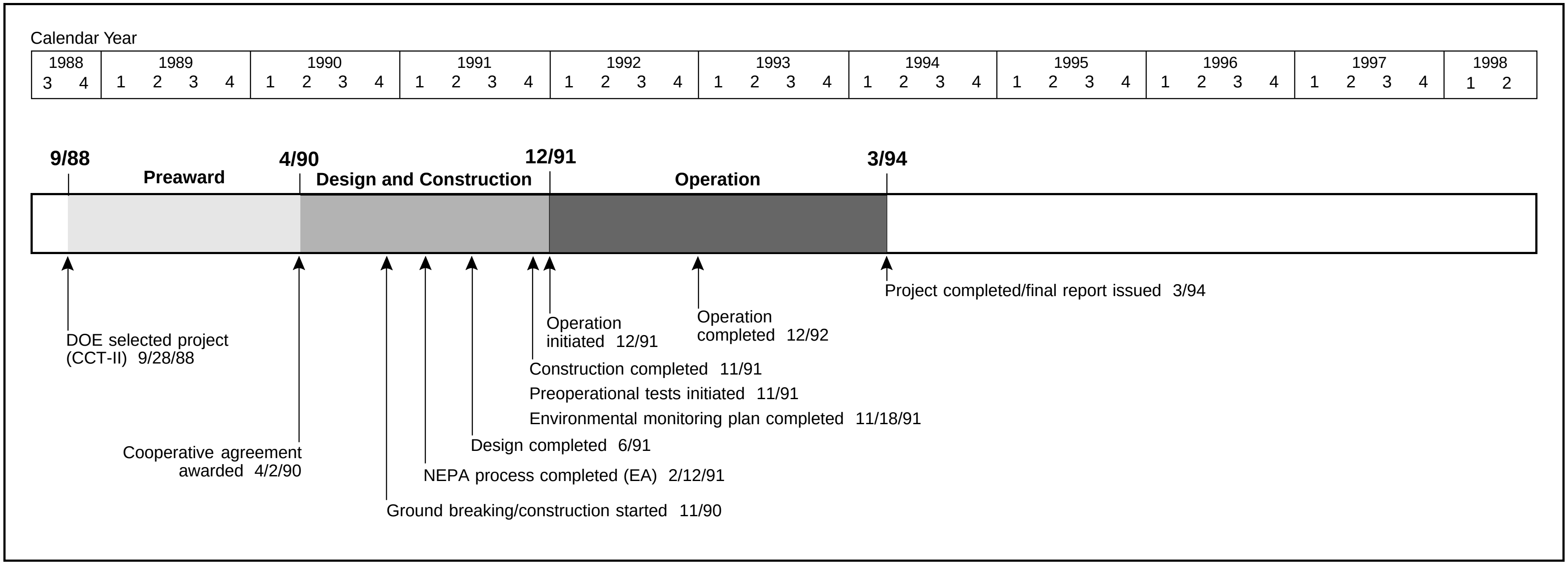
Total project cost	$13,646,609	100%
DOE	6,340,788	46
Participant	7,305,821	54

Project Objective
To demonstrate the technical and economic feasibility of achieving greater than 50% reduction in NO_x emissions with no serious impact on cyclone combustor operation, boiler performance, or other emission streams.

Technology/Project Description
Babcock & Wilcox Coal Reburn reduces NO_x in the furnace through the use of multiple combustion zones. The main combustion zone uses 70–80% of the total heat-equivalent fuel input to the boiler and slightly less than normal combustion air input. The balance of the coal (20–30%), along with significantly less than the theoretically determined requirement of air, is fed to the reburning zone above the cyclones to create an oxygen-deficient condition. The NO_x formed in the cyclone burners reacts with the resultant reducing flue gas and is converted into nitrogen in this zone. The completion of the combustion process occurs in the third zone, called the burnout zone, where the balance of the combustion air is introduced.

Coal Reburn can be applied with the cyclone burners operating within their normal, noncorrosive, oxidizing conditions, thereby minimizing any adverse effects of reburn on the cyclone combustor and boiler performance.

This project involved retrofitting an existing 100-MWe cyclone boiler that is representative of a large population of cyclone units.



Results Summary

Environmental

- Coal Reburn achieved greater than 50% NO_x reduction at full load with Lamar bituminous and PRB subbituminous coals.
- Reburn-zone stoichiometry had the greatest effect on NO_x control.
- Gas recirculation was vital to maintaining reburn-zone stoichometry while providing necessary burner cooling, flame penetration, and mixing.
- Opacity levels and electrostatic precipitator (ESP) performance were not affected by Coal Reburn with either coal tested.
- Optimal Coal Reburn heat input was 29–30% at full load and 33–35% at half to moderate loads.

Operational

- No major boiler performance problems were experienced with Coal Reburn operations.
- Boiler turndown capability was 66%, exceeding the 50% goal.
- ESP efficiency improved slightly during Lamar coal testing and did not change with PRB coal.
- Coal fineness levels above the nominal 90% through 200 mesh were maintained, reducing unburned carbon losses (UBCL).
- UBCL was the only major contributor to boiler efficiency loss, which was 0.1, 0.25, and 1.5% at loads of 110-, 82-, and 60-MWe, respectively, when using Lamar coal. With PRB coal, the efficiency loss ranged from zero at full load to 0.3% at 60-MWe.
- Superior flame stability was realized with PRB coal, contributing to better NO_x control than with Lamar coal.
- Expanded volumetric fuel delivery with reburn burners enabled switching to PRB low-rank coal without boiler derating.

Economic

- Capital costs for 110- and 605-MWe plants were $66/kW and $43/kW, respectively. Levelized 10- and 30-year busbar power costs for a 110-MWe plant were 2.4 and 2.3 mills/kWh, respectively. Levelized 10- and 30-year busbar power costs for a 605-MWe plant were 1.6 and 1.5 mills/kWh, respectively. (Costs are in 1990 constant dollars.)

Project Summary

Although cyclone boilers represent only 15% of the pre-NSPS coal-fired generating capacity, they contribute 21% of the NO_x formed by pre-NSPS coal-fired units. This is due to the cyclone combustor's inherent turbulent, high-temperature combustion process. Consequently, cyclone boilers are targeted for NO_x reduction under the CAAA and state implementation plans. However, at the time of this demonstration, there was no cost-effective combustor modification available for NO_x control.

Babcock & Wilcox Coal Reburn offers an economic and operationally sound response to the environmental impetus. This technology avoids cyclone combustor modification and associated performance complications and provides an alternative to other cyclone boiler NO_x control options having relatively higher capital and/or operating costs.

The majority of the testing was performed firing Illinois Basin bituminous coal (Lamar), as it is typical of the coal used by many utilities operating cyclones. Sub-bituminous PRB coal tests were performed to evaluate the effect of coal switching on reburn operation. Wisconsin Power and Light's strategy to meet Wisconsin's sulfur emission limitations as of January 1, 1993, was to fire low-sulfur coal.

Environmental Performance

Three sequences of testing of Coal Reburn used Lamar coal. Parametric optimization testing was used to set up the automatic controls. Performance testing was run with the unit in full automatic control at set load points. Long-term testing was performed with reburn in operation while the unit followed system load demand requirements. PRB coal was tested by parametric optimization and performance modes. Exhibit 5-19 shows changes in NO_x emissions and boiler efficiency using the reburn system for various load conditions and coal types.

Coal Reburn tests on both the Lamar and PRB coals indicated that variation of reburn-zone stoichiometry was the most critical factor in changing NO_x emissions levels. The reburn-zone stoichiometry can be varied by alternating the air flow quantities (oxygen availability) to the reburn burners, the percent reburn heat input, the gas recirculation flow rate, or the cyclone stoichiometry.

Hazardous air pollutant (HAP) testing was performed using Lamar test coal. HAP emissions were generally well within expected levels, and emissions with Coal Reburn were comparable to baseline operation. No major effect of reburn on trace-metals partitioning was discernible. None of the 16 targeted polynuclear aromatic semi-volatile organics (controlled under Title III of CAAA) was present in detectable concentrations, at a detection limit of 1.2 parts per billion.

Operational Performance

For Lamar coal, the full-, medium-, and low-load UBCL were 0.1, 0.25, and 1.5% higher, respectively, than the baseline. Full-, medium-, and low-load UBCL with PRB coal were 0.0, 0.2, and 0.3% higher, respectively, than the baseline. Coal Reburn burner flame stability improved with PRB coal.

During Coal Reburn operation with Lamar coal, the operators continually monitored boiler internals for increased ash deposition and the on-line performance monitoring system for heat transfer changes. At no time throughout the system optimization or long-term operation period were any slagging or fouling problems observed. In fact, during scheduled outages, internal boiler inspections revealed that boiler cleanliness had actually improved. Extensive ultrasonic thickness measurements were taken of the furnace wall tubes. No observable decrease in wall tube thickness was measured.

Exhibit 5-19
Coal Reburn Test Results

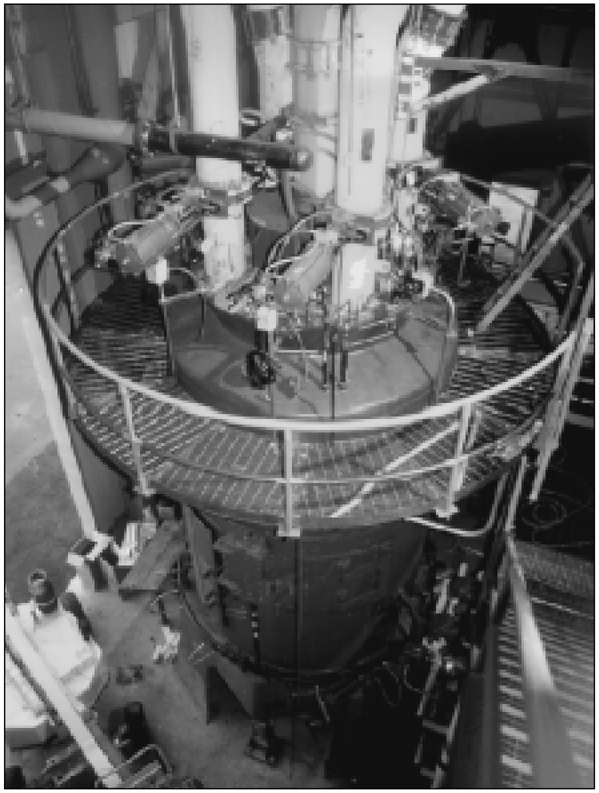
	Boiler Load 110-MWe	82-MWe	60-MWe
Lamar coal			
NO_x (lb/10^6 Btu/% reduction)	0.39/52	0.36/50	0.44/36
Boiler efficiency losses due to unburned carbon (%)	0.1	0.25	1.5
Powder River Basin coal			
NO_x (lb/10^6 Btu/% reduction)	0.34/55	0.31/52	0.30/53
Boiler efficiency losses due to unburned carbon (%)	0.0	0.2	0.3

▲ Wisconsin Power and Light Company's Nelson Dewey Station hosted the successful demonstration of Coal Reburn.

Another significant finding was that Coal Reburn minimizes and possibly eliminated a 0–25% derating normally associated with switching to subbituminous coal in a cyclone unit. This derating was a result of using a lower Btu fuel in a cyclone with a limited coal feed capacity. The reburn system transferred about 30% of the coal feed out of the cyclone to the reburn burners, bringing the cyclone feed rate down to a manageable level, while maintaining full-load heat input to the unit.

Economic Performance

An economic analysis of total capital and levelized revenue requirements was conducted using the "Electric Power Research Institute Economic Premises" for retrofit of 110- and 605-MWe plants. In addition, annualized costs per ton of NO_x removed were developed for 110- and 605-MWe plants over both 10 and 30 years. The



▲ The coal pulverizer is part of Babcock & Wilcox Coal Reburn. This system has been retained by Wisconsin Power and Light for NO_x emission control at the Nelson Dewey Station.

results of these analyses are shown in Exhibit 5-20. These values assumed typical retrofit conditions and did not take into account any fuel savings from use of low-rank coal. The pulverizers and associated coal handling were taken into account. Site-specific parameters that can significantly impact these retrofit costs included the state of the existing control system, availability of flue gas recirculation, space for coal pulverizers, space for reburn burners and overfire air ports within the boiler, scope of coal-handling modification, sootblowing capacity, ESP capacity, steam temperature control capacity, and boiler circulation considerations.

Commercial Applications

Coal Reburn is a retrofit technology applicable to a wide range of utility and industrial cyclone boilers. The current U.S. Coal Reburn market is estimated to be approximately 26,000-MWe and to consist of about 120 units ranging from 100- to 1,750-MWe with most in the 100–300-MWe range.

The project technology has been retained by Wisconsin Power and Light for commercial use.

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References

- *Demonstration of Coal Reburning for Cyclone Boiler NO_x Control: Final Project Report.* Report No. DOE/PC/89659-T16. The Babcock & Wilcox Company. February 1994. (Available from NTIS as DE94013052, Appendix 1 as DE94013053, Appendix 2 as DE94013054.)
- *Public Design Report: Coal Reburning for Cyclone Boiler NO_x Control.* The Babcock & Wilcox Company. August 1991. (Available from NTIS as DE92012554.)
- *Comprehensive Report to Congress on the Clean Coal Program: Demonstration of Coal Reburning for Cyclone Boiler NO_x Control.* (The Babcock & Wilcox Company). Report No. DOE/FE-0157. U.S. Department of Energy. February 1990. (Available from NTIS as DE90008111.)

Exhibit 5-20
Coal Reburn Economics
(1990 Constant Dollars)

Costs	Plant Size 110-MWe	605-MWe
Total capital cost ($/kW)	66	43
Levelized busbar power cost (mills/kWh)		
10-year life	2.4	1.6
30-year life	2.3	1.5
Annualized cost ($/ton of NO_x removed)		
10-year life	1,075	408
30-year life	692	263

Full-Scale Demonstration of Low-NO_x Cell Burner Retrofit

Project completed.

Participant

The Babcock & Wilcox Company

Additional Team Members

The Dayton Power and Light Company—cofunder and host
Electric Power Research Institute—cofunder
Ohio Coal Development Office—cofunder
Tennessee Valley Authority—cofunder
New England Power Company—cofunder
Duke Power Company—cofunder
Allegheny Power System—cofunder
Centerior Energy Corporation—cofunder

Location

Aberdeen, Adams County, OH (Dayton Power and Light Company's J.M. Stuart Plant, Unit No. 4)

Technology

The Babcock & Wilcox Company's low-NO_x cell burner (LNCB®) system

Plant Capacity/Production

605-MWe

Coal

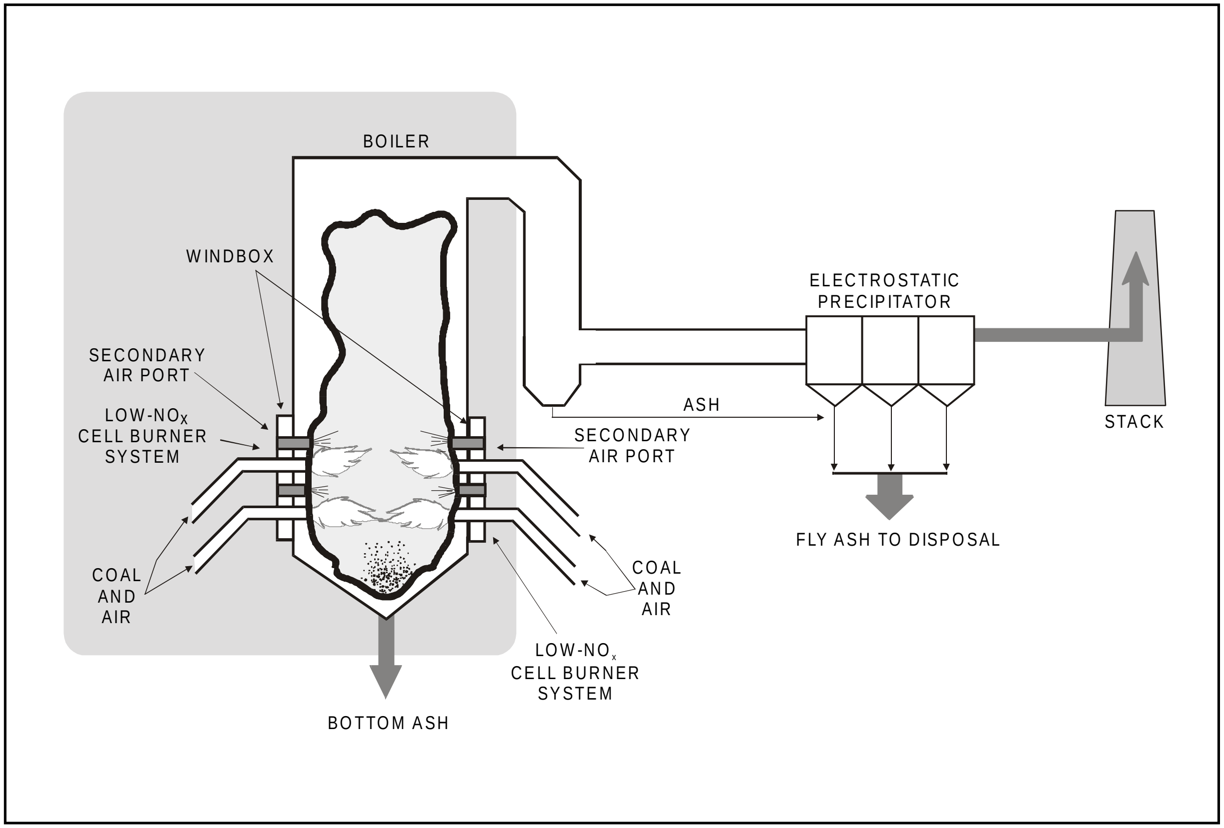
Bituminous, medium sulfur

Project Funding

Total project cost	$11,233,392	100%
DOE	5,442,800	48
Participant	5,790,592	52

Project Objective

To demonstrate, through the first commercial-scale full burner retrofit, the cost-effective reduction of NO_x from a large baseload coal-fired utility boiler with LNCB® technology; to achieve at least a 50% NO_x reduction without degradation of boiler performance at less cost than that of conventional low-NO_x burners.

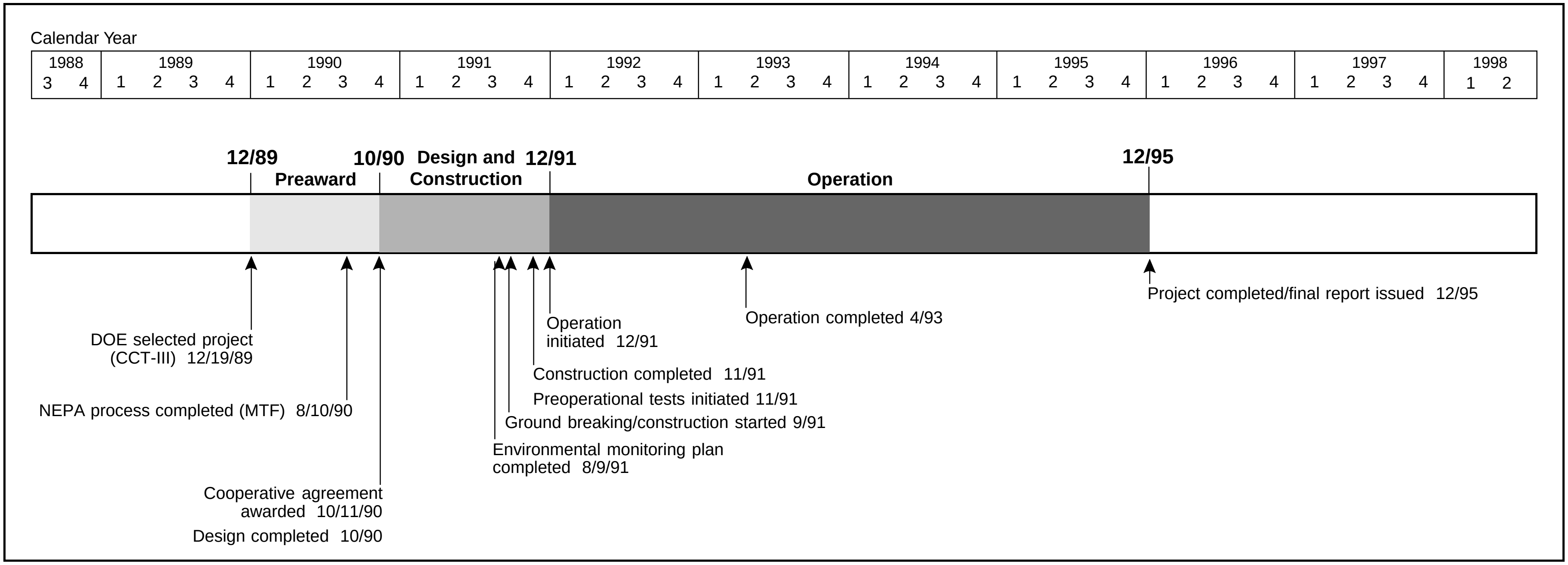


Technology/Project Description

The LNCB® technology replaces the upper coal nozzle of the standard two-nozzle cell burner with a secondary air port. The lower burner coal nozzle is enlarged to the same fuel input capacity as the two standard coal nozzles. The LNCB® operates on the principle of staged combustion to reduce NO_x emissions. Approximately 70% of the total air (primary, secondary, and excess air) is supplied through or around the coal-feed nozzle. The remainder of the air is directed to the upper port of each cell to complete the combustion process. The fuel-bound nitrogen compounds are converted to nitrogen gas, and the reduced flame temperature minimizes the formation of thermal NO_x.

The demonstration was conducted on a Babcock & Wilcox-designed, supercritical, once-through boiler equipped with an electrostatic precipitator (ESP). This unit, which is typical of cell burner boilers, contained 24 two-nozzle cell burners arranged in an opposed-firing configuration. Twelve burners (arranged in two rows of six burners each) were mounted on each of two opposing walls of the boiler. All 24 standard cell burners were removed, and 24 new LNCB® were installed. Alternate LNCB® on the bottom rows were inverted, with the air port then being on the bottom to ensure complete combustion in the lower furnace.

LNCB is a registered trademark of The Babcock & Wilcox Company.



Results Summary

Environmental

- Short-term optimization testing (all mills in service) showed NO_x reductions in the range of 53.0–55.5%, 52.5–54.7%, and 46.9–47.9% at loads of 605-MWe, 460-MWe, and 350-MWe, respectively.
- Long-term testing at full load (all mills in service) showed an average NO_x reduction of 58% (over 8 months).
- Long-term testing at full load (one mill out of service) showed an average NO_x reduction of 60% (over 8 months).
- CO emissions averaged 28–55 ppm at full load with LNCB® in service.
- Fly ash increased, but ESP performance remained virtually unchanged.

Operational

- Unit efficiency remained essentially unchanged.
- Unburned carbon losses (UBCL) increased by approximately 28% for all tests, but boiler efficiency loss was offset by a decrease in dry gas loss due to a lower boiler economizer outlet gas temperature.
- Boiler corrosion with LNCB® was roughly equivalent to boiler corrosion rates prior to retrofit.

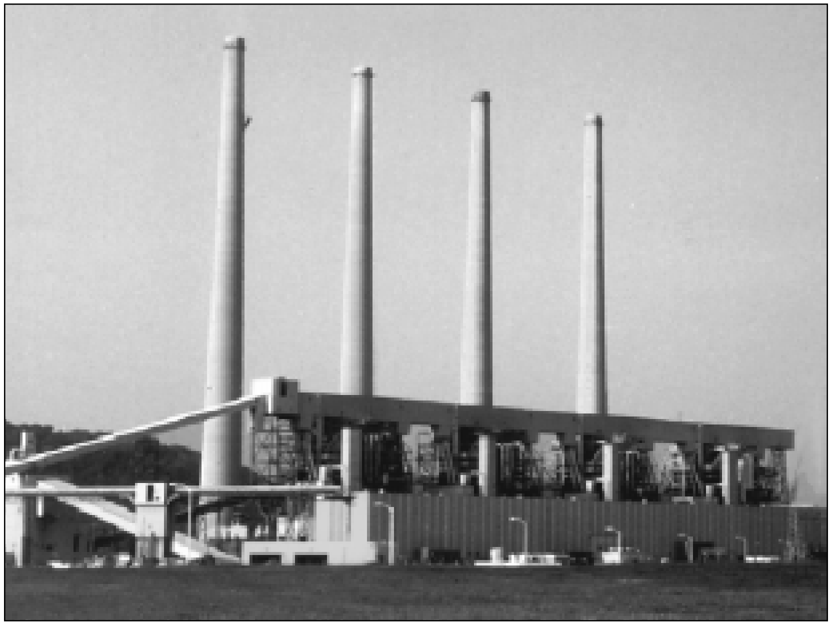
Economic

- Capital cost for a 600-MWe plant was $9/kW (1994 $).
- Levelized cost for a 600-MWe plant was estimated at 0.284 mills/kWh and $96.48/ton of NO_x removed.

Project Summary

Utility boilers equipped with cell burners currently comprise 13% or approximately 23,000-MWe of pre-NSPS coal-fired generating capacity. Cell burners are designed for rapid mixing of the fuel and air. The tight burner spacing and rapid mixing minimize the flame size while maximizing the heat release rate and unit efficiency. Combustion efficiency is good, but the rapid heat release produces relatively large quantities of NO_x.

To reduce NO_x emissions, the LNCB® has been designed to stage mixing of the fuel and combustion air. A key design criterion was accomplishing delayed fuel-air mixing with no modifications to waterwall panels. A plug-in design reduces material costs and outage time required to complete the retrofit, compared to installing conventional, internally staged low-NO_x burners. LNCB® provides a lower cost alternative to address NO_x reduction requirements for cell burners.



▲ Dayton Power and Light Company's J.M. Stuart Plant hosted the successful demonstration of LNCB® technology.

Environmental Performance

The initial LNCB® configuration resulted in excessive CO and H_2S emissions. Through modeling, a revised configuration was developed to address the problem without compromising boiler performance. The modification was incorporated and validated model capabilities.

Following parametric testing to establish optimal operating modes, a series of optimization tests were conducted on the LNCB® to assess environmental and operational performance. Two sets of measurements were taken, one by Babcock & Wilcox and the other by an independent company, to validate data accuracy. Consequently, the data provided is a range reflecting the two measurements.

The average NO_x emissions reduction achieved at full load with all mills in service ranged from 53.0–55.5%. With one mill out of service at full load, the average NO_x reduction ranged from 53.3–54.5%.

Average NO_x reduction at intermediate load (about 460-MWe) ranged from 52.5–54.7%. At low loads (about 350-MWe), average NO_x reduction ranged from 46.9–47.9%.

NO_x emissions were monitored over the long-term at full load for all mills in service and one mill out of service. Each test spanned an 8-month period. NO_x emission reductions realized were 58% for all mills in service and about 60% for one mill out of service.

Complications arose in assessing CO emissions relative to baseline because baseline calibration was not refined enough. However, accurate measurements were made with LNCB® in service. CO emissions were corrected to 3.0% O_2 and measured at full, intermediate, and low loads. The range of CO emissions at full load with all mills in service was 28–55 ppm and 20-38 ppm with one mill out of service. At intermediate loads (about 460-MWe), CO emissions were 28–45 ppm and at low loads (about 350-MWe), 5–27 ppm.

Particulate emissions were minimally impacted. The LNCB® had little effect on flyash resistivity, largely due to SO_3 injection, and therefore ESP removal efficiency remained very high. Baseline ESP collection efficiencies for full load with all mills in service, full load with one mill in service, and intermediate load with one mill out of service were 99.5, 99.49, and 99.81%, respectively. For the same conditions, in the same sequence with LNCB® in operation, ESP collection efficiencies were 99.43, 99.12, and 99.35%, respectively.

▲ The LNCB® is viewed from within the boiler.

Operational Performance

Furnace exit gas temperature, or secondary superheater inlet temperature, initially decreased by 100 ºF but eventually rose to within 10 ºF of baseline conditions.

The UBCL increased by approximately 28% for all tests. The most significant increase from baseline data occurred for a test with one mill out of service. A 52% increase in UBCL resulted in an efficiency loss of 0.69%.

Boiler efficiency showed very little change from baseline. The average for all mills in service increased by 0.16%. The higher post-retrofit efficiency was attributed to a decrease in dry gas loss with lower economizer gas outlet temperature (and subsequent lower air heater gas outlet temperature), offsetting UBCL and CO emission losses. Also, increased coal fineness mitigated UBCL.

Because sulfidation is the primary corrosion mechanism in substoichiometric combustion of sulfur-containing coal, H_2S levels were monitored in the boiler. After optimizing LNCB® operation, levels were largely at the lower detection limit. There were some higher local readings, but corrosion panel tests established that corrosion rates with LNCB® were roughly equivalent to pre-retrofit rates.

Ash sample analyses indicated that ash deposition would not be a problem. The LNCB® ash was little different from baseline ash. Furthermore, the small variations observed in furnace exit gas temperature between baseline and LNCB® indicated little change in furnace slagging. Start-up and turndown of the unit were unaffected by conversion to LNCB®.

Economic Performance

The economic analyses were performed for a 600-MWe nominal unit size and typical location in the midwest United States. A medium-sulfur, medium-volatile bituminous coal was chosen as the typical fuel. For a baseline NO_x emission level of 1.2 lb/10^6 Btu and a 50% reduction target, the estimated capital cost was $9/kW (1994 $). The levelized cost of electricity was estimated at 0.284 mills/kWh or $96.48/ton of NO_x removed.

Commercial Applications

The low cost and short outage time for retrofit make the LNCB® design the most cost-effective NO_x control technology available today for cell burner boilers. The LNCB® system can be installed at about half the cost and time of other commercial low-NO_x burners.

Dayton Power & Light has retained the LNCB® for use in commercial service. Seven commercial contracts have been awarded for 172 burners, valued at $27 million. LNCB® have already been installed on more than 4,600-MWe of capacity.

The project received *R&D* magazine's 1994 R&D Award.

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References

- *Final Report: Full-Scale Demonstration of Low-NO_x Cell Burner Retrofit.* Report No. DOE/PC/90545-T2. The Babcock & Wilcox Company. December 1995. (Available from NTIS as DE96003766.)
- *Public Design Report: Full-Scale Demonstration of Low-NO_x Cell Burner Retrofit*. Report No. DOE/PC/90545-T4. The Babcock & Wilcox Company. August 1991. (Available from NTIS as DE92009768.)
- *Comprehensive Report to Congress on the Clean Coal Technology Program: Full-Scale Demonstration of Low-NO_x Cell-Burner Retrofit.* The Babcock & Wilcox Company. Report No. DOE/FE-0197P. U.S. Department of Energy. July 1990. (Available from NTIS as DE90018026.)

▲ The connections to the LNCB® are viewed from outside the boiler.

Evaluation of Gas Reburning and Low-NO_x Burners on a Wall-Fired Boiler

Project completed.

Participant
Energy and Environmental Research Corporation

Additional Team Members
Public Service Company of Colorado—cofunder and host
Gas Research Institute—cofunder
Colorado Interstate Gas Company—cofunder
Electric Power Research Institute—cofunder
Foster Wheeler Energy Corp.—technology supplier

Location
Denver, Adams County, CO (Public Service Company of Colorado's Cherokee Station, Unit No. 3)

Technology
Energy and Environmental Research Corporation's gas-reburning (GR) system
Foster Wheeler Energy Corp.'s Low-NO_x burners (LNB)

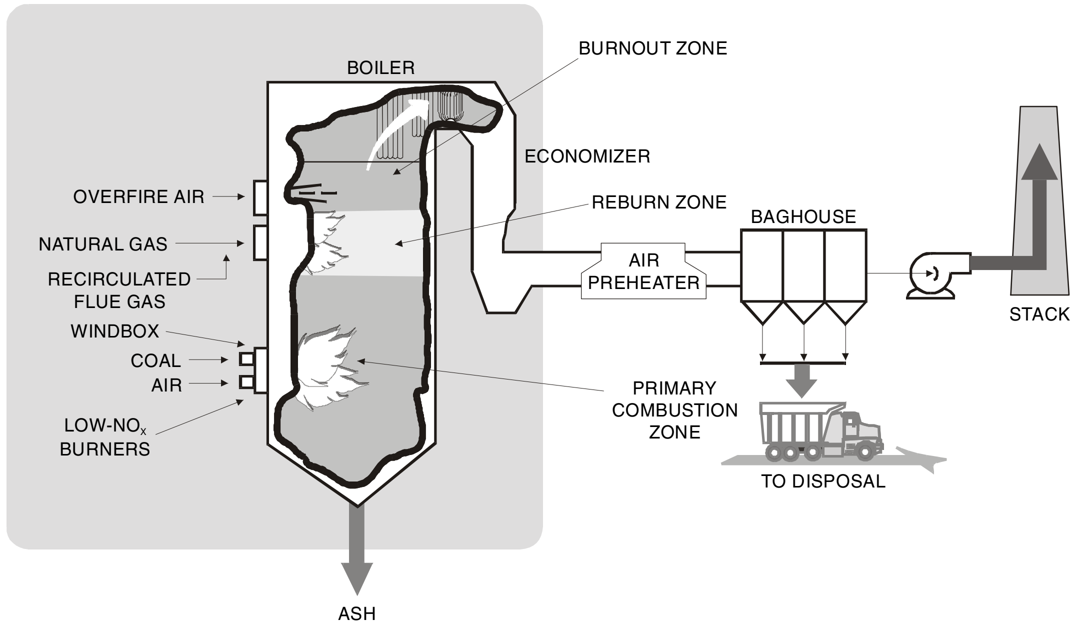
Plant Capacity/Production
172-MWe (gross), 158-MWe (net)

Coal
Colorado bituminous, 0.40% sulfur

Project Funding

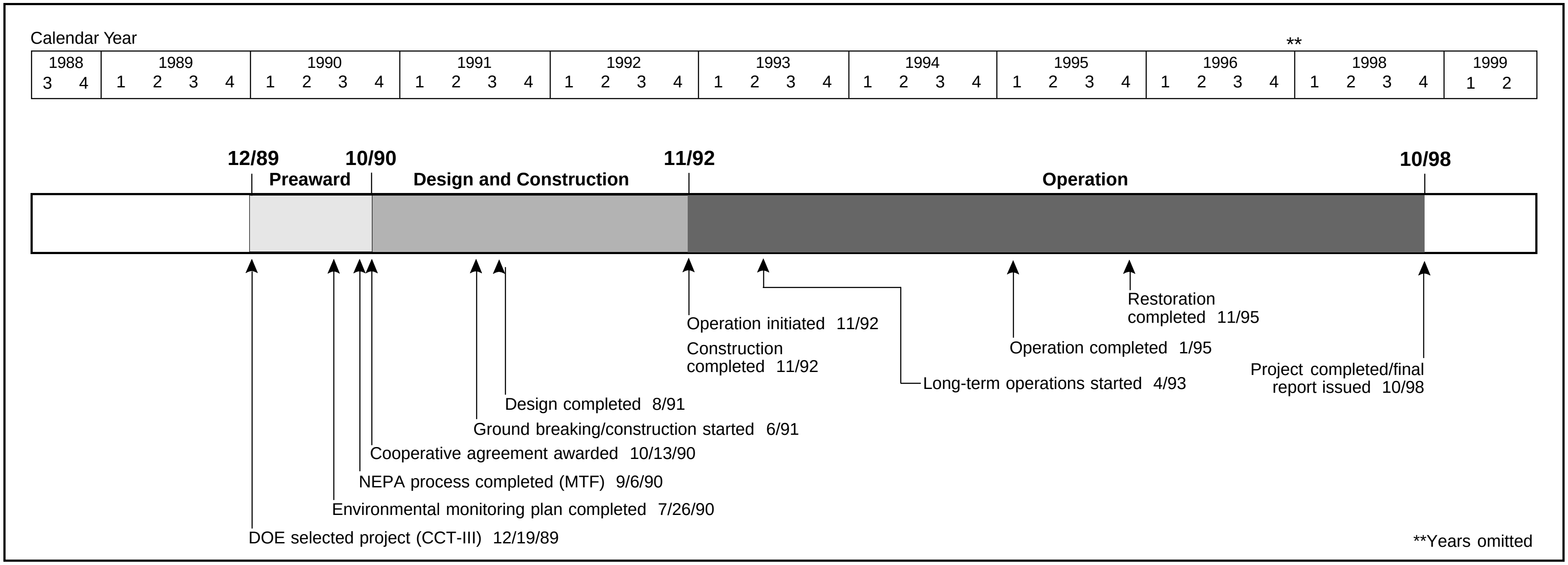
Total project cost	$17,807,258	100%
DOE	8,895,790	50
Participant	8,911,468	50

Project Objective
To attain up to a 70% decrease in the emissions of NO_x from an existing wall-fired utility boiler firing low-sulfur coal using both gas reburning and low-NO_x burners (GR–LNB); and to assess the impact of GR–LNB on boiler performance.



Technology/Project Description
Gas reburning involves firing natural gas (up to 25% of total heat input) above the main coal combustion zone in a boiler. This upper-level firing creates a slightly fuel-rich zone. NO_x drifting upward from the lower region of the furnace is "reburned" in this zone and converted to molecular nitrogen. Low-NO_x burners positioned in the coal combustion zone retard the production of NO_x by staging the burning process so that the coal-air mixture can be carefully controlled at each stage. The synergistic effect of adding a reburning stage to wall-fired boilers equipped with low-NO_x burners was intended to lower NO_x emissions by up to 70%. Gas reburning was demonstrated with and without the use of recirculated flue gas and with optimized overfire air.

A series of parametric tests were performed on the gas reburning system, varying operational control parameters, and assessing the effect on boiler emissions, completeness of combustion (carbon-in-ash), thermal efficiency, and heat rate. A one-year long-term testing program was performed in order to judge the consistency of system outputs, assess the impact of long-term operation on the boiler equipment, gain experience in operating GR–LNB in a normal load-following environment, and develop a database for use in subsequent GR–LNB applications. Both first- and second-generation gas-reburning tests were performed.



Results Summary

Environmental

- LNB alone reduced NO_x emissions from a pre-construction baseline of 0.73 lb/10^6 Btu to 0.48 lb/10^6 Btu, a 37% NO_x reduction.
- First-generation GR, which incorporated flue gas recirculation, in combination with LNB, reduced NO_x emissions to 0.25 lb/10^6 Btu, a 66% NO_x reduction at an 18% gas heat input rate.
- Second-generation GR, without flue gas recirculation, in combination with LNB reduced NO_x emissions to 0.26 lb/10^6 Btu, a 64% NO_x reduction with only 12.5% gas heat input.
- Both first- and second-generation GR with LNB were capable of reducing NO_x emissions by up to 70% for short periods of time, the average was 65%.
- After modifying the overfire air system to enhance penetration and turbulence (as part of second-generation GR), CO emissions were controlled to acceptable levels at low gas heat input rates (5–10%).
- SO_2 emissions and particulate loadings were reduced by the percentage heat input supplied by GR.

Operational

- Boiler efficiency decreased by approximately 1.0%.
- There was no measurable boiler tube wear and only a small amount of slagging.
- Carbon-in-ash on CO levels were acceptable for first- and second-generation GR with LNB, but not LNB alone.

Economic

- Capital cost for GR–LNB retrofit is $26.01/kW (1996$) plus the gas pipeline cost, if not in place, for 300-MWe plant ($12.14/kW for GR only and $13.87/kW for LNB only)
- Operating costs were related to the gas/coal cost differential and the value of SO_2 emission allowances (because GR reduces SO_2 emissions when displacing coal).

Project Summary

The demonstration established that GR–LNB offers a cost-effective option for deep NO_x reduction on wall-fired boilers. GR–LNB NO_x control performance approached that of selective catalytic reduction (SCR) but at significantly lower cost. The importance of cost-effective technology for deep NO_x reduction is reflected in ongoing deliberations on the need for NO_x reduction in ozone nonattainment areas beyond what is currently projected in Title IV of the CAAA. Title I of the CAAA deals with ozone nonattainment and is currently the driving force for deep NO_x reduction in many regions of the country.

The GR–LNB was installed and evaluated on a 172-MWe (gross) wall-fired boiler—a balanced-draft pulverized-coal unit supplied by Babcock & Wilcox. The GR system, including an overfire air system, was designed and installed by Energy and Environmental Research Corporation. The LNBs were designed and installed by

Foster Wheeler Energy Corp.

Parametric testing was begun in October 1992 and completed in April 1993. The parametric tests were conducted by changing the process variables (such as zone stoichiometric ratio, percent gas heat input, percent overfire air, and load) and the effects of these variables on NO_x reduction, SO_2 reduction, CO emissions, carbon-in-ash, and heat rates were analyzed. The baseline condition of the LNB was also established.

Environmental Performance

At a constant load (150-MWe) and a constant oxygen level at the boiler exit, both NO_x and SO_2 emissions decreased when natural gas was introduced in the GR operation. In general, the NO_x emissions were reduced with increasing gas heat input. At gas heat inputs greater than 10%, NO_x emissions were reduced marginally as gas heat input increased. Natural gas also reduced SO_2 emissions in proportion to the gas heat input. At Cherokee Station, low-sulfur (0.40%) coal was used, and typical SO_2 emissions were 0.65 lb/10^6 Btu. With a gas heat input of 20%, SO_2 emissions decreased by 20% to 0.52 lb/10^6 Btu.

The CO_2 emissions were also reduced as a result of using natural gas because it has a lower carbon-to-hydrogen ratio than coal. At a gas heat input of 20%, the CO_2 emissions were reduced by 8%.

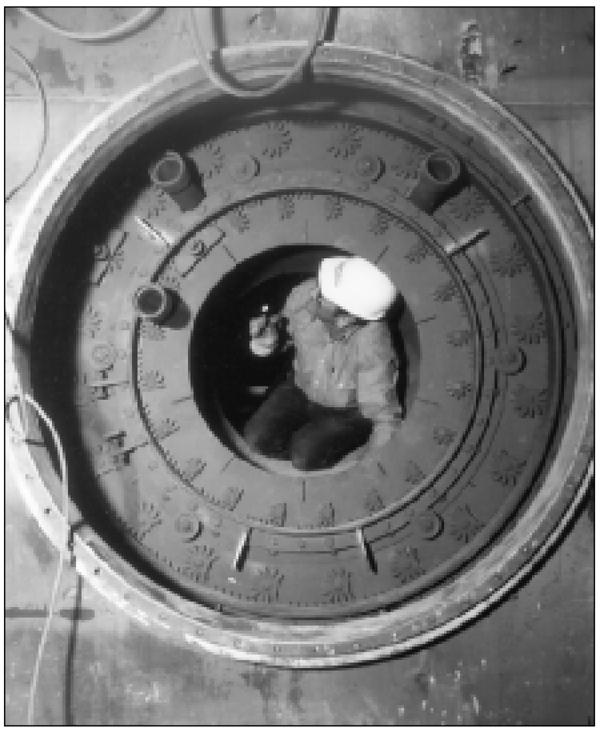
Long-term testing was initiated in April 1993 and completed in January 1995. The objectives of the test were to obtain operating data over an extended period when the unit was under routine commercial service, determine the effect of GR–LNB operation on the unit, and obtain incremental maintenance and operating costs with GR. During long-term testing, it was determined that flue gas recirculation had minimal effect on NO_x emissions.

A second series of tests were added to the project to evaluate a modified or second-generation system. Modifications are summarized below:

- The flue gas recirculation system, originally designed to provide momentum to the natural gas, was removed. (This change significantly reduced capital costs.)
- Natural gas injection was optimized at 10% gas heat input compared to the initial design value of 18%. The removal of the flue gas recirculation system required installation of high-velocity injectors, which made greater use of available natural gas pressure. (This modification reduced natural gas usage and thus operating costs.)
- Overfire air ports were modified to provide higher jet momentum, especially at low total flows.

Over 4,000 hours of operation were achieved, with the results as shown in Exhibit 5-21.

Although the 37% NO_x reduction performance of LNB was less than the expected 45%, the overall objectives of the demonstration were met. Boiler efficiency decreased by only 1% during gas reburning due to increased moisture in the fuel resulting from natural gas use. Further, there was no measurable tube wear, and only small amounts of slagging occurred during the GR–LNB demonstration. However, with LNB alone, carbon-in-ash and CO could not be maintained at acceptable levels.



▲ A worker inspects the support ring for the Foster Wheeler low-NO_x burner installed in the boiler wall.

Exhibit 5-21
NO_x Data from Cherokee Station, Unit No. 3

	GR Generation	
	First	Second
Baseline (lb/10^6 Btu)	0.73	0.73
Avg NO_x reduction (%)		
LNB	37	44
GR–LNB	65	64
Avg gas heat input (%)	18	12.5

Economic Performance

GR–LNB is a retrofit technology in which the economic benefits are dependent on the following site-specific factors:

- Gas availability at the site
- Gas/coal cost differential
- Boiler efficiency
- SO_2 removal requirements
- Value of SO_2 emission credits

Based on the demonstration, GR–LNB is expected to achieve at least 64% NO_x control with a gas heat input of 12.5%. The capital cost estimate for a 300-MWe wall-fired installation is \$26.01/kW (1996 \$) plus gas pipeline costs, if required. This cost includes both equipment and installation costs and a 15% contingency. The GR and LNB system capital costs can be easily separated from one another because they are independent systems. The capital cost for the GR system only is estimated at \$12.14/kW. The LNB system capital cost is \$13.87/kW.

Operating costs are almost entirely related to the differential cost of natural gas and coal and reduced by the value of the SO_2 emission credits received due to absence of sulfur in the gas. Gas costs more than coal on a \$/Btu basis, so a differential cost of \$1.00/10^6 Btu was used. Boiler efficiency was estimated to decline by 0.80%; the cost of this decline was calculated using a composite fuel cost of \$1.67/10^6 Btu. Over-fire air boaster and cooling fans auxiliary loads will be partially offset by lower loads on the pulverizers. No additional operating labor is required, but there is an increase in maitenance costs. Allowances were also made for overhead, taxes, and insurance. Based on these assumptions and assuming an SO_2 credit allowance of \$95/ton (Feb. 1996), the net operating cost is \$2.14 million per year.

Commercial Applications

Current estimates indicate that about 35 existing wall-fired utility installations, plus industrial boilers, could make immediate use of this technology. The technology can be used in retrofit, repowering, or greenfield installations. There is no known limit to the size or scope of the application of this technology combination.

GR–LNB is expected to be less capital intensive, or less costly, than a scrubber, selective catalytic reduction, or other technologies. GR–LNB functions equally well with any kind of coal.

Public Service Company of Colorado, the host utility, decided to retain the low-NO_x burners and the gas-reburning system for immediate use; however, a restoration was required to remove the flue gas recirculation system.

Energy and Environmental Research Corporation has been awarded two contracts to provide gas-reburning systems for five cyclone coal-fired boilers: TVA's Allen Unit No. 1, with options for Unit Nos. 2 and 3, (identical 330-MWe Units); Baltimore Gas & Electric's C.P. Crane, Unit No. 2, with an option for Unit No. 1, (similar 200-MWe Units). Start-up of the first two units is planned for mid-1998.

This project was one of two that received the Air and Waste Management Association's 1997 J. Deanne Sensenbaugh Award.

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References

- *Evaluation of Gas Reburning and Low NO_x Burners on a Wall-Fired Boiler: Performance and Economics Report, Gas Reburning-Low NO_x Burner System, Cherokee Station Unit No. 3, Public Service Company of Colorado.* Final Report. July 1998.
- *Guideline Manual: Gas Reburning—Low NO_x Burner System,* Cherokee Station Unit No. 3, Public Service Company of Colorado. Final Report. July 1998.
- *Evaluation of Gas Reburning and Low NO_x Burners on a Wall-Fired Boiler (Long-Term Testing, April 1993–January 1995).* Report No. DOE/PC/90547-T20. Energy and Environmental Research Corporation. June 1995. (Available from NTIS as DE95017755.)
- *Evaluation of Gas Reburning and Low NO_x Burners on a Wall-Fired Boiler (Optimization Testing, November 1992–April 1993).* Report No. DOE/PC/90547-T19. Energy and Environmental Research Corporation. June 1995. (Available from NTIS as DE95017754.)
- *Comprehensive Report to Congress on the Clean Coal Technology Program: Evaluation of Gas Reburning and Low-NO_x Burners on a Wall-Fired Boiler.* Energy and Environmental Research Corporation. Report No. DOE/FE-0204P. U.S. Department of Energy. September 1990. (Available from NTIS as DE9100253.)

▲ The Public Service Company of Colorado has retained the gas-reburning and low-NO_x burner system for commercial use.

Demonstration of Selective Catalytic Reduction Technology for the Control of NO_x Emissions from High-Sulfur-Coal-Fired Boilers

Project completed.

Participant
Southern Company Services, Inc.

Additional Team Members
Electric Power Research Institute—cofunder
Ontario Hydro—cofunder
Gulf Power Company—host

Location
Pensacola, Escambia County, FL (Gulf Power Company's Plant Crist, Unit No. 4)

Technology
Selective catalytic reduction (SCR)

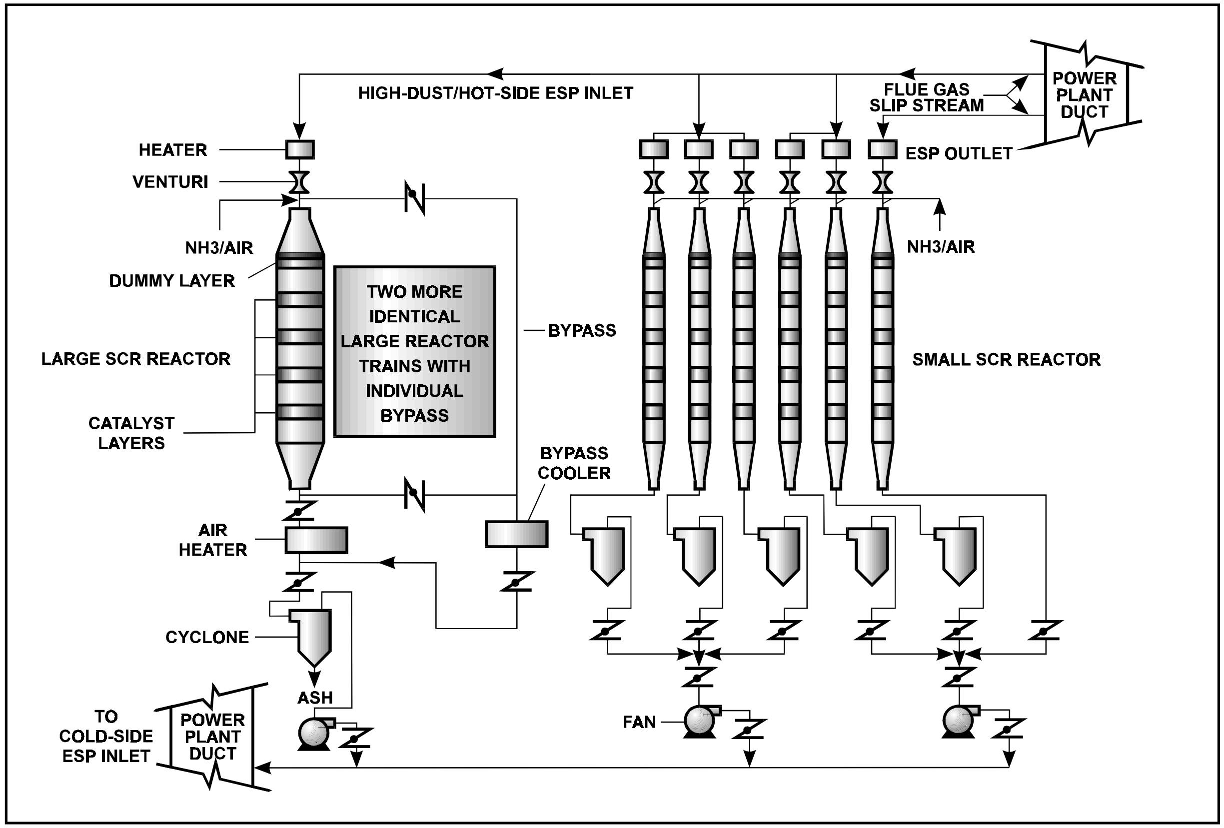
Plant Capacity/Production
8.7-MWe equivalent (three 2.5-MWe and six 0.2-MWe equivalent SCR reactor plants)

Coal
Illinois bituminous, 2.7% sulfur

Project Funding

Total project cost	$23,229,729	100%
DOE	9,406,673	40
Participant	13,823,056	60

Project Objective
To evaluate the performance of commercially available SCR catalysts when applied to operating conditions found in U.S. pulverized coal-fired utility boilers using high-sulfur U.S. coal under various operating conditions while achieving as much as 80% NO_x removal.



Technology/Project Description
The SCR technology consists of injecting ammonia into boiler flue gas and passing it through a catalyst bed where the NO_x and ammonia react to form nitrogen and water vapor.

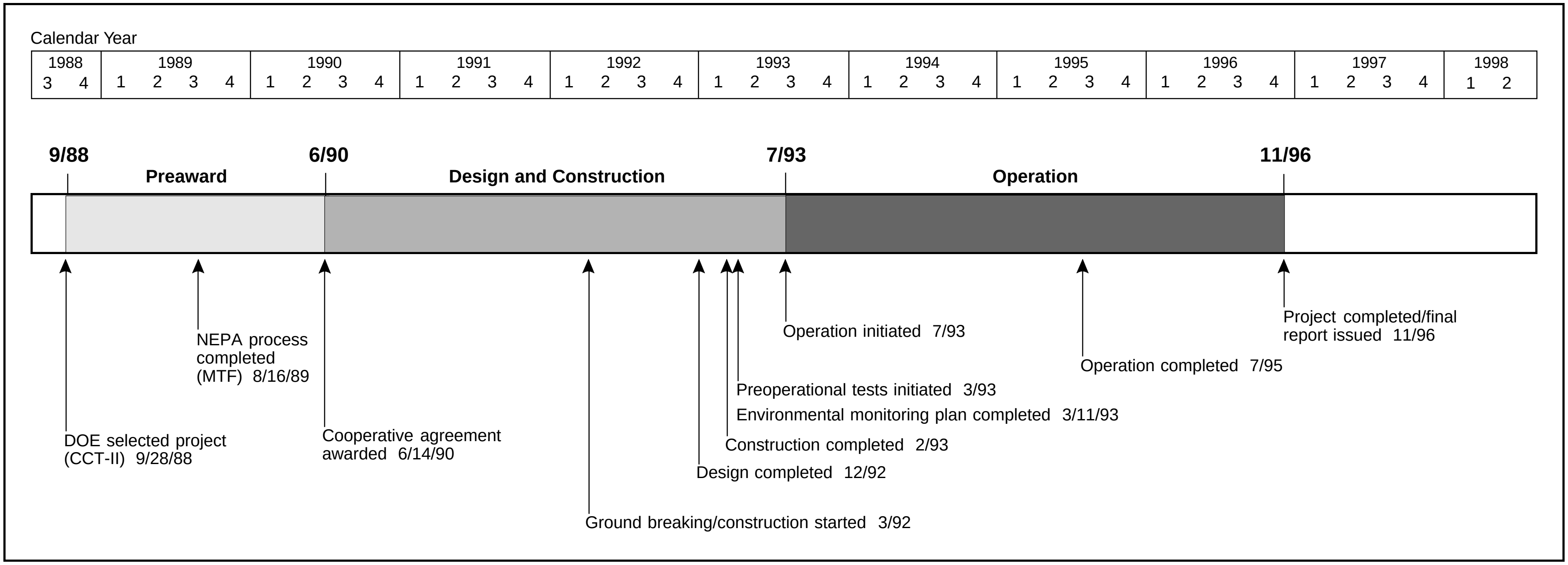
In this demonstration project, the SCR facility consisted of three 2.5-MWe equivalent SCR reactors, supplied by separate 5,000 scfm flue gas slipstreams, and six 0.20-MWe equivalent SCR reactors. These reactors were calculated to be large enough to produce design data that will allow the SCR process to be scaled up to commercial size. Catalyst suppliers (two U.S., two European, and two Japanese) provided eight catalysts with various shapes and chemical compositions for evaluation of process chemistry and economics of operation during the demonstration.

The project demonstrated, at high- and low-dust loadings of flue gas, the applicability of SCR technology to provide a cost-effective means of reducing NO_x emissions from power plants burning high-sulfur U.S. coal.

The demonstration plant, which was located at Gulf Power Company's Plant Crist near Pensacola, FL, used flue gas from the burning of 2.7% sulfur coal under various NO_x and particulate levels.

Results Summary

Environmental
- NO_x reductions of over 80% were achieved at an ammonia slip well under the 5 ppm acceptable for commercial operation.



- Flow rates could be increased to 150% of design without exceeding the ammonia slip design level of 5 ppm at 80% NO_x reduction.
- While catalyst performance increased above 700 ºF, the benefit did not outweigh the heat rate penalties.
- The increase for ammonia slip, a sign of catalyst deactivation, went from less than 1 ppm to approximately 3 ppm over the nearly 12,000 hours of operation, thus demonstrating deactivation in coal-fired units was in line with worldwide experience.
- Long-term testing showed that SO_2 oxidation was within or below the design limits necessary to protect downstream equipment.

Operational

- Fouling of catalysts was controlled by adequate sootblowing procedures.
- Long-term testing showed that catalyst erosion was not a problem.
- Air preheater performance was degraded because of ammonia slip and subsequent by-product formation; however, solutions were identified.
- The SCR process did not significantly affect the results of Toxicity Characteristic Leaching Procedure analysis of the fly ash.

Economic

Levelized costs for various NO_x removal levels for a 250-MWe unit at 0.35 lb/10^6 Btu inlet follow:

	40%	60%	80%
1996 levelized cost (mills/kWh)	2.39	2.57	2.79
1996 levelized cost ($/ton)	3,502	2,500	2,036

Project Summary

The demonstration tests were designed to address several uncertainties, including potential catalyst deactivation due to poisoning by trace metals species in U.S. coals, performance of technology and effects on the balance-of-plant equipment in the presence of high amounts of SO_2 and SO_3, and performance of the SCR catalyst under typical U.S. high-sulfur coal-fired utility operating conditions. Catalyst suppliers were required to design the catalyst baskets to match predetermined reactor dimensions, provide a maximum of four catalyst layers, and meet the following reactor baseline conditions:

Parameter	Minimum	Baseline	Maximum
Temperature (ºF)	620	700	750
NH_3/NO_x molar ratio	0.6	0.8	1.0
Space velocity (1% design flow)	60	100	150
Flow rate (scfm)			
Large reactor	3,000	5,000	7,500
Small reactor	240	400	600

The catalysts tested are listed in Exhibit 5-22. Catalyst suppliers were given great latitude in providing the amount of catalyst for this demonstration.

Exhibit 5-22
Catalysts Tested

Catalyst	Reactor Size*	Catalyst Configuration
Nippon/Shokubai	Large	Honeycomb
Siemens AG	Large	Plate
W.R. Grace/Noxeram	Large	Honeycomb
W.R. Grace/Synox	Small	Honeycomb
Haldor Topsoe	Small	Plate
Hitachi/Zosen	Small	Plate
Cormetech/High dust	Small	Honeycomb
Cormetech/Low dust	Small	Honeycomb

* Large = 2.5-MWe; 5,000 scfm   Small = 0.2-MWe; 400 scfm

Environmental Results

Ammonia slip, the controlling factor in the long-term operation of commercial SCR, was usually ≤5 ppm because of plant and operational considerations. Ammonia slip was dependent on catalyst exposure time, flow rate, temperature, NH_3/NO_x distribution, and NH_3/NO_x ratio (NO_x reduction). Changes in NH_3/NO_x ratio and consequently NO_x reduction generally produced the most significant changes in ammonia slip. The ammonia slip at 60% NO_x reduction was at or near the detection limit of 1 ppm. As NO_x reduction was increased above 80%, ammonia slip also increased and remained at reasonable levels up to NO_x reductions of 90%. Over 90%, the ammonia slip levels increased dramatically.

The flow rate and temperature effects on NO_x reduction were also measured. In general, flows could be increased to 150% of design without the ammonia slip exceeding 5 ppm at 80% NO_x reduction and design temperature. With respect to temperature, most catalysts exhibited fairly significant improvements in overall performance as temperatures increased from 620 °F to 700 °F but relatively little improvement as temperature increased from 700 °F to 750 °F. The conclusion was that the benefits of high-temperature operation probably do not outweigh the heat rate penalties involved in operating SCR at the higher temperatures.

Catalyst deactivation was generally observed by an increase in ammonia slip over time, assuming the NO_x reduction efficiency was held constant. Over the 12,000 hours of the demonstration tests, the ammonia slip did, in fact, increase from less than 1 ppm to approximately 3 ppm. These results demonstrated the maturity of catalyst design and that deactivation was in line with prior worldwide experience.

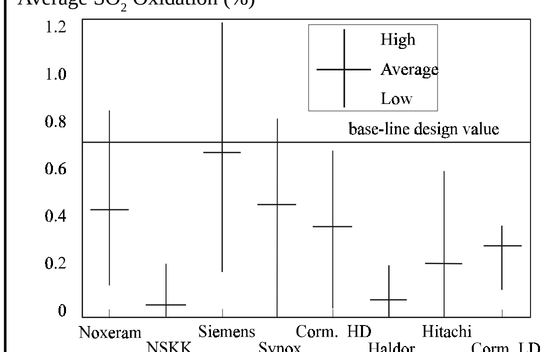
It has been observed that the catalytic active species that results in NO_x reduction often contributed to SO_2 oxidation (i.e., SO_3 formation), which can be detrimental to downstream equipment. In general, NO_x reduction can be increased as the tolerance for SO_3 is also increased. The upper bound for SO_2 oxidation for the demonstration catalyst was set at 0.75% at baseline conditions. The average SO_2 oxidation rate for each of the catalysts is shown in Exhibit 5-23. These data reflect baseline conditions over the life of the demonstration. All of the catalysts were within design limits, with most exhibiting oxidation rates below the design limit. Other factors affecting SO_2 oxidations are listed below:

- **Flow Rate.** Most of the catalysts exhibited fairly constant SO_2 oxidation with respect to flow rate (i.e., space velocity). In theory, SO_2 oxidation should be inversely proportional to flow rate.
- **Temperature.** Theoretically, the relationship between SO_2 oxidation and temperature should be exponential as temperature increases; however, measurements showed the relationship to be linear with little difference in SO_2 oxidation between 620 ºF and 700 ºF. On the other hand, between 700 °F and 750 °F, the SO_2 oxidation increased more significantly.

Other Findings

- **Pressure Drop.** Overall reactor pressure drop was a function of the catalyst geometry and volume, but tests to determine which one was controlling were inconclusive.
- **Fouling.** The fouling characteristics of the catalyst were important to long-term operation. During the demonstration, measurements showed relatively level pressure drop over time, indicating that sootblowing procedures were effective. The plate-type configurations had somewhat less fouling potential than did the honeycomb configuration, but both were acceptable for application.
- **Erosion.** Catalyst erosion was not considered to be a significant problem because most of the erosion was attributed to aggressive sootblowing.

Exhibit 5-23
Average SO_2 Oxidation Rate
(Baseline)



NH_3/NO_x = 0.8, 700 ºF, design flow

- **Air Preheater Performance.** The demonstration showed that the SCR process exacerbated performance degradation of the air preheaters mainly due to ammonia slip and subsequent by-product formation. Regenerator-type air heaters outperformed recuperators in SCR applications in terms of both thermal performance and fouling.
- **Ammonia Volatilization.** The ammonia volatilized from the SCR flyash when a significant amount of water was absorbed by the ash. This was caused by the formation of a moist layer on the ash with a pH high enough to convert the ammonia compounds in the ash to gas-phase ammonia.
- **Toxicity Characteristic Leaching Procedure (TCLP) Analysis.** TCLP analyses were performed on flyash samples. The SCR process did not significantly affect the toxics leachability of the fly ash.

Economic Results

An economic evaluation was performed for full-scale applications of SCR technology to a new 250-MWe pulverized coal-fired plant located in a rural area with minimal space limitations. The fuel considered was high-sulfur Illinois No. 6 coal. Other key base case design criteria are shown in Exhibit 5-24.

Results of the economic analysis of capital, operating and maintenance (O&M), and levelized cost based on a 30-year project life for various unit sizes for an SCR system with a NO_x removal efficiency of 60% follow:

	125-MWe	250-MWe	700-MWe
Capital cost ($/kW)	61	54	45
Operating cost ($)	580,000	1,045,000	2,667,000
1996 levelized cost			
mills/kWh	2.89	2.57	2.22
$/ton	2,811	2,500	2,165

Results of the economic analysis of capital, O&M, and levelized cost for various NO_x removal efficiencies for a 250-MWe unit with 0.35 lb/10^6 Btu of inlet NO_x are as follows:

	40%	60%	80%
Capital cost ($/kW)	52	54	57
Operating costs ($)	926,000	1,045,000	1,181,000
1996 levelized cost			
mill/kWh	2.39	2.57	2.79
$/ton	3,502	2,500	2,036

For retrofit applications, the estimated capital costs were $59–112/kW, depending on the size of the installation and the difficulty and scope of the retrofit. The levelized costs for the retrofit applications were $1,850–5,100/ton (current 1996 $).

Exhibit 5-24
Design Criteria

Parameter	Specification
Type of SCR	Hot side
Number of reactors	One
Reactor configuration	3 catalyst support layers
Initial catalyst load	2 of 3 layers loaded
Range of operation	35–100% boiler load
NO_x inlet concentration	0.35 lb/10^6 Btu
Design NO_x reduction	60%
Design ammonia slip	5 ppm
Catalyst life	16,000 hr
Ammonia cost	$250/ton
SCR cost	$400/ft^3

Commercial Applications

As a result of this demonstration, SCR technology has been shown to be applicable to existing and new utility generating capacity for removal of NO_x from the flue gas of virtually any size boiler. There are approximately 1,041 coal-fired utility boilers in active commercial service in the United States; these boilers represent a total generating capacity of 296,000-MWe.

Contacts

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James U. Watts, FETC, (412) 892-5991

References

- *Control of Nitrogen Oxide Emissions: Selective Catalytic Reduction (SCR).* Topical Report No. 9. U.S. Department of Energy and Southern Company Services, Inc. July 1997.
- Maxwell, J. D., et al. "Demonstration of SCR Technology for the Control of NO_x Emissions from High-Sulfur Coal-Fired Utility Boilers." *Fifth Annual Clean Coal Technology Conference: Technical Papers,* January 1997.
- *Demonstration of SCR Technology for the Control of NO_x Emissions from High-Sulfur Coal-Fired Utility Boilers: Final Report.* Vol. 1. Southern Company Services, Inc. October 1996. (Available from NTIS, Vol. 1 as DE97050873, Vol. 2: Appendixes A–N as DE97050874, and Vol. 3: Appendixes O–T as DE97050875.)
- *Economic Evaluation of Commercial-Scale SCR Applications for Utility Boilers.* Southern Company Services, Inc. September 1996. (Available from NTIS as DE97051156.)

180-MWe Demonstration of Advanced Tangentially Fired Combustion Techniques for the Reduction of NO_x Emissions from Coal-Fired Boilers

Project completed.

Participant

Southern Company Services, Inc.

Additional Team Members

Gulf Power Company—cofunder and host

Electric Power Research Institute—cofunder

ABB Combustion Engineering, Inc.—cofunder and technology supplier

Location

Lynn Haven, Bay County, FL (Gulf Power Company's Plant Lansing Smith, Unit No. 2)

Technology

ABB Combustion Engineering's Low-NO_x Concentric Firing System (LNCFS™) with advanced overfire air (AOFA), clustered coal nozzles, and offset air

Plant Capacity/Production

180-MWe

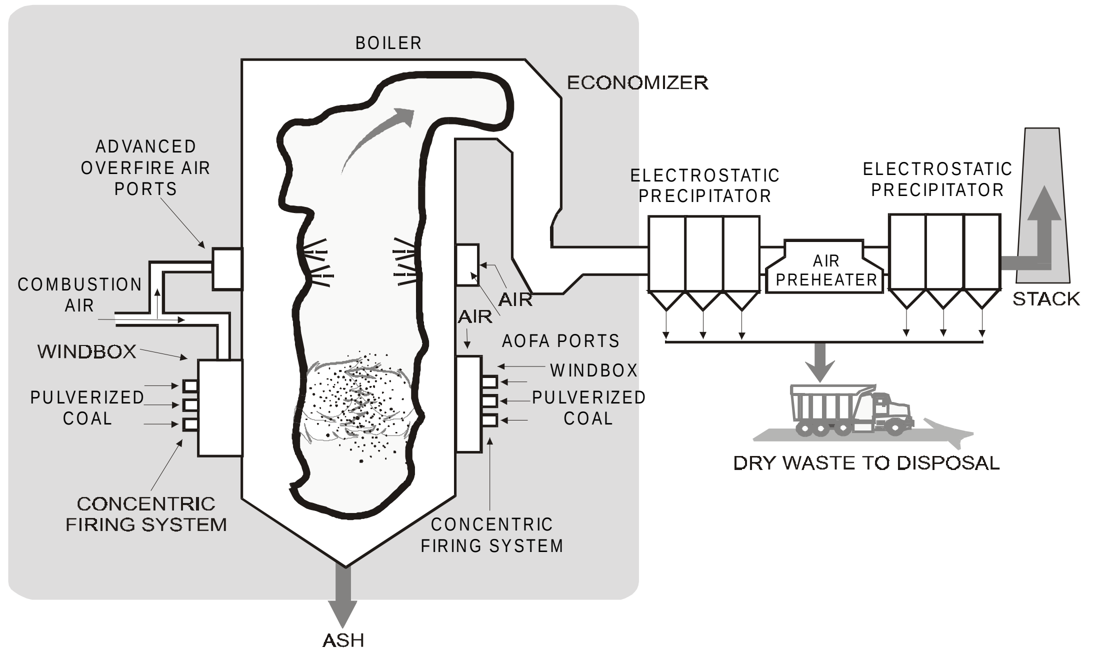
Coal

Eastern bituminous, high reactivity

Project Funding

Total project cost	$9,153,383	100%
DOE	4,440,184	49
Participant	4,713,199	51

LNCFS is a trademark of ABB Combustion Engineering, Inc.



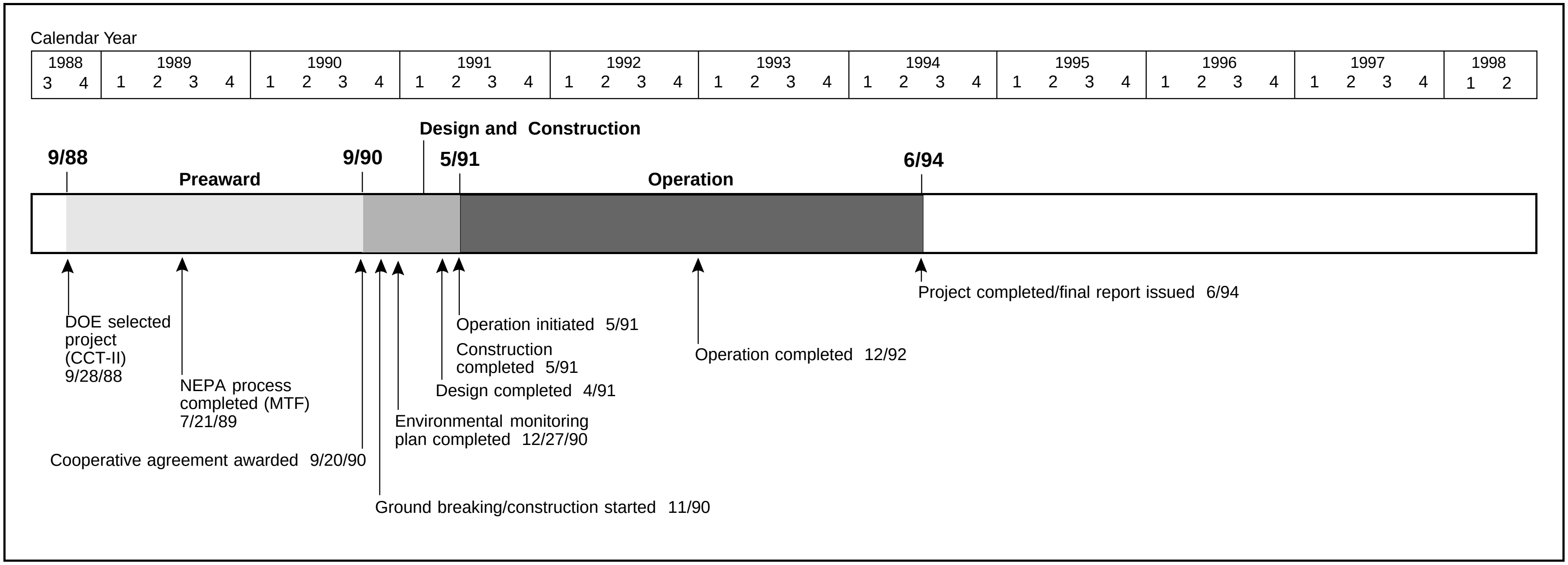
Project Objective

To demonstrate in a stepwise fashion the short- and long-term NO_x reduction capabilities of Low-NO_x Concentric Firing System (LNCFS™) levels I, II, and III on a single reference boiler.

Technology/Project Description

Technologies demonstrated included the LNCFS™ levels I, II, and III. Each level of the LNCFS™ used different combinations of overfire air and clustered coal nozzle positioning to achieve NO_x reductions. With the LNCFS™, primary air and coal are surrounded by oxygen-rich secondary air that blankets the outer regions of the combustion zone. LNCFS™ I used a close-coupled overfire air (CCOFA) system integrated directly into the windbox of the boiler. A separated overfire air (SOFA) system located above the combustion zone was featured in the LNCFS™ II system. This was an advanced overfire air system that incorporates back pressuring and flow measurement capabilities. CCOFA and SOFA were both used in the LNCFS™ III tangential-firing approach.

Carefully controlled short-term tests were conducted followed by long-term testing under normal load dispatch conditions. Long-term tests, which typically lasted 2–3 months for each phase, best represent the true emissions characteristics of each technology. Results presented are based on long-term test data.



Results Summary

Environmental

- At full load, the NO_x emissions using LNCFS™ I, II, and III were 0.39, 0.39, and 0.34 lb/10^6 Btu, respectively, which represent reductions of 37, 37, and 45% from the baseline emissions.
- Emissions with LNCFS™ were not sensitive to power outputs between 100- and 200-MWe, but emissions increased significantly below 100-MWe, reaching baseline emission levels at 70-MWe.
- Because of reduced effectiveness at low loads, LNCFS™ proved marginal as a compliance option for peaking load conditions.
- Average CO emissions increased at full load.
- Air toxics testing found LNCFS™ to have no clear-cut effect on the emissions of trace metals or acid gases. Volatile organic compounds (VOCs) appeared to be reduced and semi-volatile compounds increased.

Operational

- Loss-on-ignition (LOI) was not sensitive to the LNCFS™ retrofits but very sensitive to coal fineness.
- Furnace slagging was reduced but back-pass fouling was increased for LNCFS™ II and III.
- Boiler efficiency and unit heat rate were impacted minimally.
- Unit operation was not significantly affected, but operating flexibility of the unit was reduced at low loads with LNCFS™ II and III.

Economic

- The capital cost estimate for LNCFS™ I was \$5–15/kW and for LNCFS™ II and III, \$15–25/kW (1993\$).
- The cost effectiveness for LNCFS™ I was \$103/ton of NO_x removed; LNCFS™ II, \$444/ton; and LNCFS™ III, \$400/ton (1993\$).

Project Summary

At the time of the demonstration, specific NO_x emission regulations were being formulated under the CAAA. The data developed over the course of this project provided needed real-time input to regulation development.

LNCFS™ technology was designed for tangentially-fired boilers, which represent a large percentage of the pre-NSPS coal-fired generating capacity. The technology reduces NO_x by staging combustion in the boiler vertically by separating coal and air injectors and horizontally by creating fuel-rich and lean zones with offset air nozzles. The objective was to determine NO_x emission reductions and impact on boiler performance over the long-term under normal dispatch and operating conditions. By using the same boiler, the demonstration provided direct comparative performance analysis of the three configurations. Short-term parametric testing enabled extrapolation of results to other tangentially fired units by evaluating the relationship between NO_x emissions and key operating parameters.

Exhibit 5-25
LNCFS™ Configurations

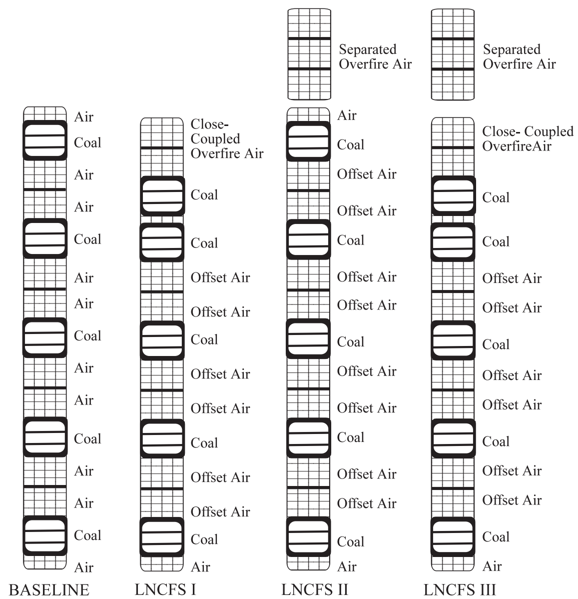


Exhibit 5-26
Concentric Firing Concept

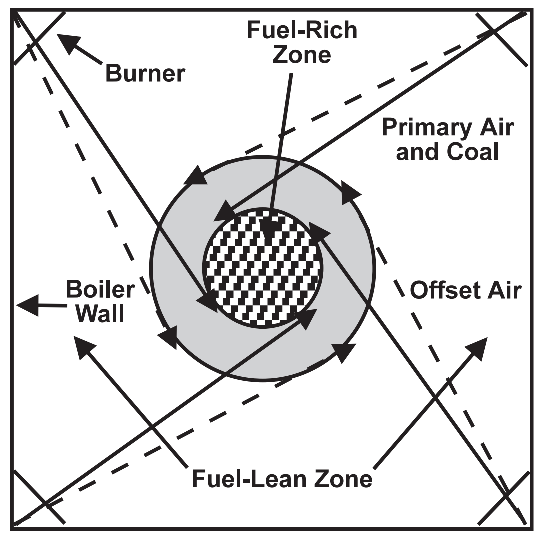


Exhibit 5-25 shows the various LNCFS™ configurations used to achieve staged combustion. In addition to overfire air, as shown in Exhibit 5-26, the LNCFS™ incorporates other NO_x-reducing techniques into the combustion process. Using offset air, two concentric circular combustion regions are formed. The majority of the coal is contained in the fuel-rich inner region. This region is surrounded by a fuel-lean zone containing combustion air. The size of this outer annulus of combustion air can be varied using adjustable offset air nozzles.

Operational Performance

Exhibit 5-27 summarizes the impacts of LNCFS™ on unit performance.

Environmental Performance

At full load, LNCFS™ I, II, and III reduced NO_x emissions by 37, 37, and 45%, respectively.

Exhibit 5-28 presents the NO_x emission estimates obtained in the assessment of the average annual NO_x emissions for three dispatch scenarios.

Air toxics testing found LNCFS™ to have no clear-cut effect on the emission of trace metals or acid gases. The data provided marginal evidence for a decreased emission of chromium. The effect on aldehydes/ketones could not be assessed because baseline data were compromised. VOCs appeared to be reduced and semi-volatile compounds increased. The increase in semi-volatile compounds was deemed to be consistent with increases in the amount of unburned carbon in the ash.

Economic Performance

LNCFS™ II was the only complete retrofit (LNCFS™ I and III were modifications of LNCFS™ II), and therefore capital cost estimates were based on the Lansing Smith Unit No. 2 retrofit as well as other tangentially-fired LNCFS™ retrofits. The capital cost ranges in 1993 constant dollars follow:

- LNCFS™ I—$5–15/kW
- LNCFS™ II—$15–25/kW
- LNCFS™ III—$15–25/kW

Site-specific considerations have a significant effect on capital costs; however, the above ranges reflect recent experience and are planning estimates. The actual capital cost for LNCFS™ II at Lansing Smith Unit No. 2 was $3 million, or $17/kW, which falls within the projected range.

The cost effectiveness of the LNCFS™ technologies is based on the capital and operating and maintenance costs and the NO_x removal efficiency of the technologies. The cost effectiveness of the LNCFS™ technologies is listed below (based on a levilization factor of 0.144 in 1993 constant dollars):

- LNCFS™ I—$103/ton of NO_x removed
- LNCFS™ II—$444/ton of NO_x removed
- LNCFS™ III—$400/ton of NO_x removed

Commercial Applications

LNCFS™ technology has been adopted by eight other utilities in eight separate retrofits over a range of capacities. Further, potential commercial applications of this technology include nearly 600 U.S. pulverized coal, tangentially fired utility units. These units range from 25-MWe to 950-MWe in size and fire a wide range of coals, from low-volatile bituminous through lignite.

LNCFS™ has been retained at the host site for commercial use. ABB Combustion Engineering has modified 116 tangentially-fired boilers, representing over 25,000 MWe, with LNCFS™ and derivative TFS 2000™ burners.

Exhibit 5-27
Unit Performance Impacts Based on Long-Term Testing

	Baseline	LNCFS™ I	LNCFS™ II	LNCFS™ III
Avg CO at full load (ppm)	10	12	22	33
Avg excess O_2 at full load (%)	3.7	3.2	4.5	4.3
LOI at full load (%) O_2 (%)	4.8 4.0	4.6 3.9	4.2 5.3	5.9 4.7
Steam outlet conditions	Satisfactory at full load; low temper-patures at low loads	Full load: 5–10 ºF lower than baseline Low loads: 10–30 ºF lower than baseline	Same as baseline	160–200-MWe: OK 80-MWe: 15–35 ºF lower than baseline
Furnace slagging and backpass fouling	Medium	Medium	Reduced slagging, but increased fouling	Reduced slagging, but increased fouling
Operating flexibility	Normal	Same as baseline	More care required at low loads	More difficult to operate than other systems
Boiler efficiency (%) Efficiency change	90 N/A	90.2 +0.2	89.7 -0.3	89.85 -0.15
Turbine heat rate (Btu/kWh)	9,000	9,011	9,000	9,000
Unit net heat rate (Btu/kWh) Change (%)	9,995 N/A	9,986 -0.1	10,031 +0.36	10,013 +0.18

Exhibit 5-28
Average Annual NO_x Emissions and Percent Reduction

Boiler Duty Cycle	Units	Baseline	LNCFS™ I	LNCFS™ II	LNCFS™ III
Baseload (161.8-MWe avg)	Avg NO_x emissions (lb/10^6 Btu) Avg reduction (%)	0.62	0.41 38.7	0.41 38.7	0.36 42.2
Intermediate load (146.6-MWe avg)	Avg NO_x emissions (lb/10^6 Btu) Avg reduction (%)	0.62	0.40 39.2	0.41 35.9	0.34 45.3
Peaking load (101.8-MWe avg)	Avg NO_x emissions (lb/10^6 Btu) Avg reduction (%)	0.59	0.45 36.1	0.47 20.3	0.43 28.0

Contacts

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References

- *180-MWe Demonstration of Advanced Tangentially Fired Combustion Techniques for the Reduction of Nitrogen Oxide (NO_x) Emissions from Coal-Fired Boilers: Final Report and Key Project Findings*. Report No. DOE/PC/89653-T14. Southern Company Services, Inc. February 1994. (Available from NTIS as DE94011174.)
- *180-MWe Demonstration of Advanced Tangentially Fired Combustion Techniques for the Reduction of Nitrogen Oxide (NO_x) Emissions from Coal-Fired Boilers—Plant Lansing Smith—Phase III and Final Environmental Monitoring Program Report.* Southern Company Services, Inc. December 1993.
- *Measurement of Chemical Emissions under the Influence of Low-NO_x Combustion Modifications*. Report No. DOE/PC/89653-T12. Southern Company Services, Inc. October 1993. (Available from NTIS as DE94005038.)
- *180-MW Demonstration of Advanced Tangentially Fired Combustion Techniques for the Reduction of Nitrogen Oxide (NO_x) Emissions from Coal-Fired Boilers: Public Design Report.* Report No. DOE/PC/89652-T13. Southern Company Services, Inc. September 1993. (Available from NTIS as DE94000218.)

Demonstration of Advanced Combustion Techniques for a Wall-Fired Boiler

Project completed.

Participant

Southern Company Services, Inc. (SCS)

Additional Team Members

Electric Power Research Institute (EPRI)—cofunder
Foster Wheeler Energy Corporation (Foster Wheeler)—technology supplier
Georgia Power Company—host

Location

Coosa, Floyd County, GA (Georgia Power Company's Plant Hammond, Unit No. 4)

Technology

Foster Wheeler's low-NO_x burner (LNB) with advanced overfire air (AOFA)

Coal

Eastern bituminous coals, 1.7% sulfur

Plant Capacity/Production

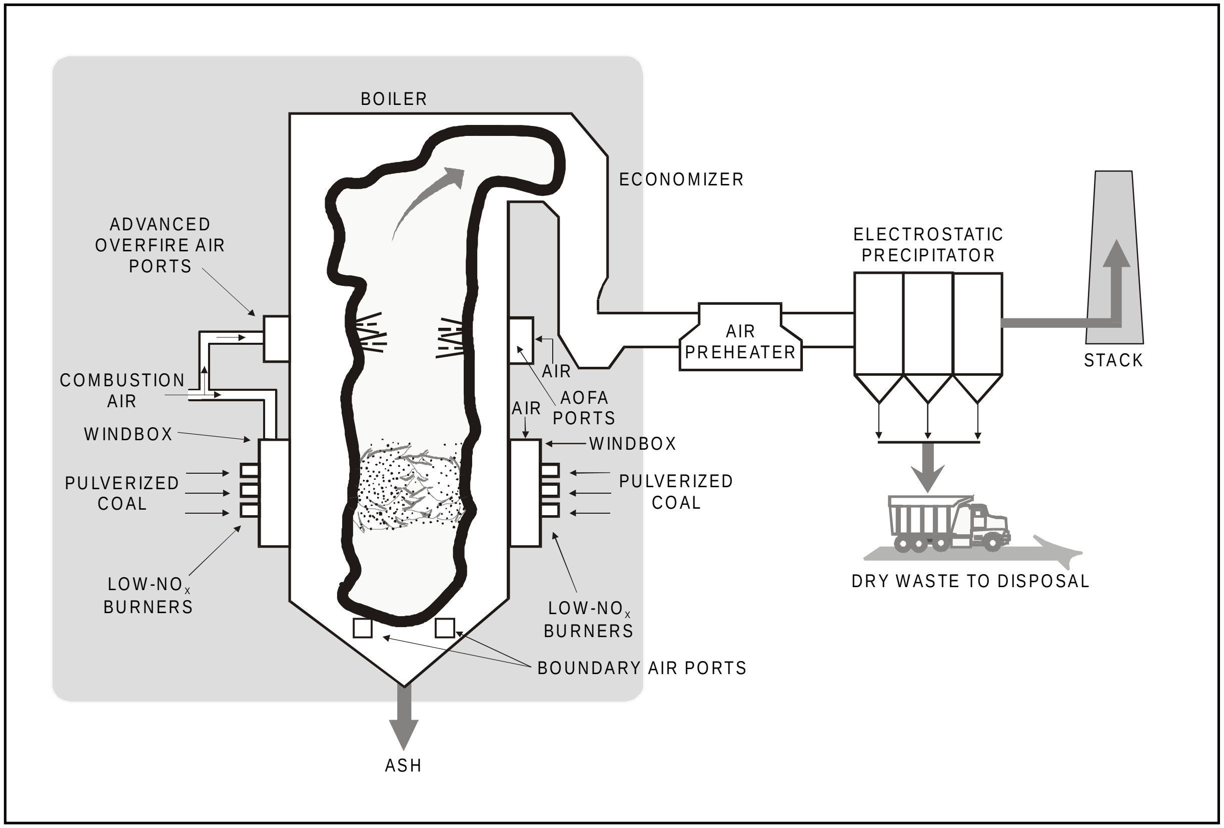
500-MWe

Project Funding

Total project cost	$15,853,900	100%
DOE	6,553,526	41
Participant	9,300,374	59

Project Objective

To achieve 50% NO_x reduction with the LNB/AOFA system; to determine the contributions of AOFA and LNB to NO_x reduction and the parameters for optimal LNB/AOFA performance; and to assess the long-term effects of LNB, AOFA, combined LNB/AOFA, and the Generic NO_x Control Intelligence System (GNOCIS) advanced digital controls on NO_x reduction and boiler performance.



Technology/Project Description

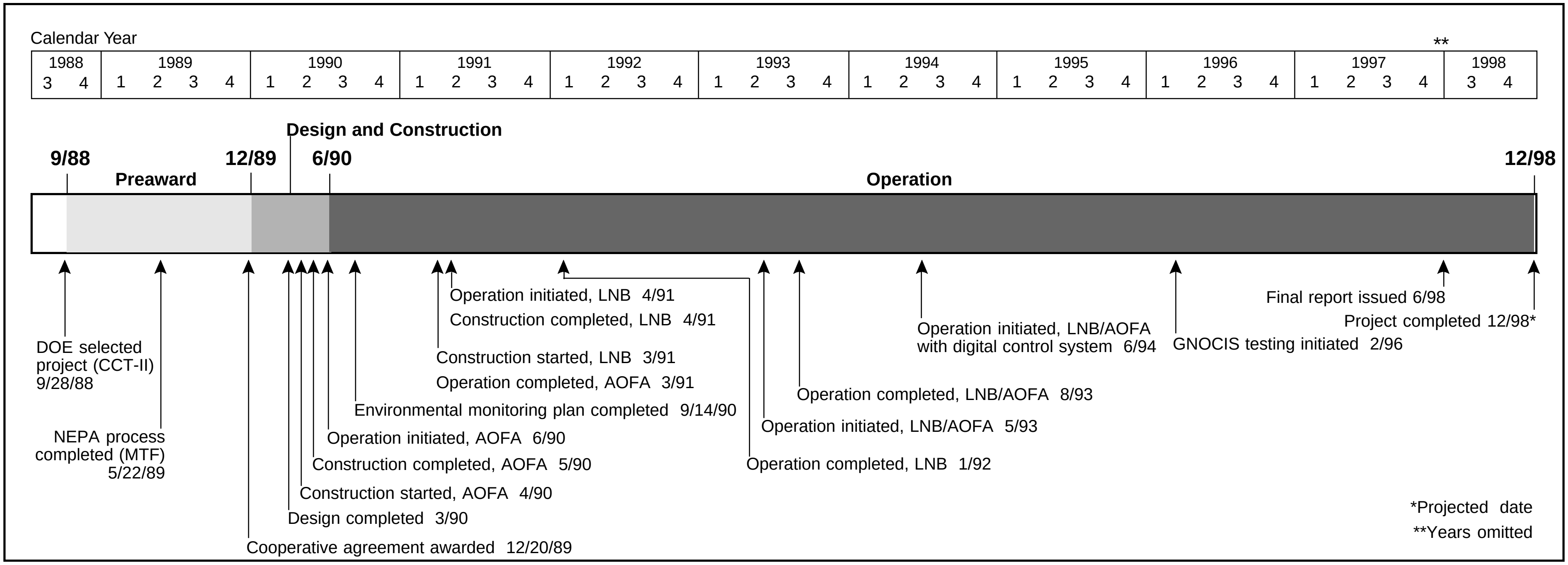
In a LNB, fuel and air mixing is controlled to mitigate the formation of NO_x by regulating the primary air-fuel mixture, velocity, and turbulence to create a fuel-rich flame core. Furthermore, by controlling the rate that secondary air, which is required to complete combustion, is mixed with flame solids and gases, an oxygen deficient atmosphere is created that reduces thermal-NO_x formation.

AOFA involves (1) improving the mixing of overfire air with the furnace gases to achieve complete combustion, (2) depleting the air from the burner zone to minimize thermal-NO_x formation, and (3) supplying air over furnace wall tube surfaces to prevent slagging and furnace corrosion. Plant Hammond Unit No. 4 is a nominal 500-MWe pulverized coal opposed wall-fired unit, which typifies many existing pre-NSPS wall-fired utility boilers in the United States.

Results Summary

Operational

- At full load, fly ash loss-on-ignition (LOI) was near 8% (compared to a baseline of 5%) for LNB alone and LNB/AOFA combined.
- AOFA accounted for an incremental NO_x reduction beyond the use of LNB of approximately 17%, with additional reductions resulting from other operational changes.



- GNOCIS achieved boiler efficiency gain of 0.5 percentage points, a reduction in fly ash LOI levels of 1-3 percentage points, and a reduction in NO_x emissions of 10-15 % at full load.

Environmental

- Using LNB alone, NO_x emissions were 0.65 lb/10^6 Btu at full load, representing a 48% reduction from baseline conditions (1.24 lb/10^6 Btu).
- Using AOFA only, NO_x reductions of 24% below baseline conditions were achieved under normal long-term operation, depending upon load.
- Using LNB/AOFA, full load NO_x emissions were approximately 0.40 lb/10^6 Btu, which represents a 68% reduction from baseline conditions.
- There was not a significant difference in emissions of trace metals, acid gases, and volatile organic compounds between AOFA and LNB/AOFA operations.

Economic

- Capital cost for a 500 MWe wall-fired unit is $8.8/kW for AOFA alone, $10.0/kW for LNB alone, and $0.5/kW for GNOCIS.
- Estimated cost of NO_x removal is $86/ton.

Project Summary

Operational

SCS conducted baseline characterization of the unit in an "as-found" condition from August 1989 to April 1990. The AOFA system was tested from August 1990 to March 1991. Following installation of the LNBs in the second quarter of 1991, the LNBs were tested from July 1991 to January 1992, excluding a three-month delay when the plant ran at reduced capacity. Post-LNB increases in fly ash LOI, along with increases in combustion air requirements and fly ash loading to the electrostatic precipitator (ESP), adversely affected the unit's stack particulate emissions. The LNB/AOFA testing was conducted from January 1992 to August 1993, excluding downtime for a scheduled outage and for portions of the test period due to excessive particulate emissions. However, an ammonia flue gas conditioning system was added to improve ESP performance, which enabled the unit to operate at full load and testing to continue.

LOI increased significantly for the AOFA, LNB, and LNB/AOFA phases despite improved mill performance due to the replacement of the mills.

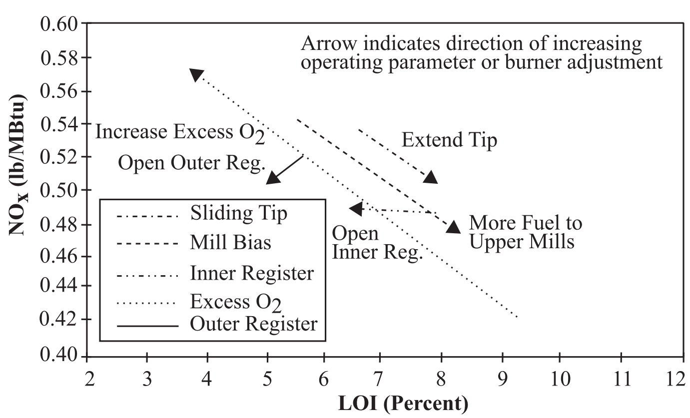
Increased LOI was a concern not only because of the associated efficiency loss, but a potential loss of fly ash sales. The increased carbon in the fly ash can render the material unsuitable for use in making concrete.

During October 1992, SCS conducted parametric testing to determine the relationship between NO_x and LOI emissions. The parameters tested were: excess oxygen, mill coal flow bias, burner sliding tip position, burner outer register position, and burner inner register position. Nitrogen oxide emissions and LOI levels varied from 0.44–0.57 lb/10^6 Btu and 3–10%, respectively. As expected, excess oxygen level had considerable effect on both NO_x and LOI. The results showed that there is some flexibility in selecting the optimum operating point and making tradeoffs between NO_x emissions and fly ash LOI; however, much of the variation was the result of changes in excess oxygen. This can be more clearly seen in Exhibit 5-29 in which all sensitivities are plotted. This exhibit shows that for excess oxygen, mill bias, inner register, and sliding tip, any adjustments to reduce NO_x emissions are at the expense of increased fly ash LOI. In contrast, the slope of the outer register characteristic suggests improvement in both NO_x emissions and LOI can be achieved by adjustment of this damper. However, due to the relatively small impact of the outer register adjustment on both NO_x and LOI, it is likely the positive NO_x/LOI slope is an artifact of process noise.

A subsidiary goal of the project was to evaluate advanced instrumentation and controls (I&C) as applied to combustion control. The need for more sophisticated I&C equipment is illustrated in Exhibit 5-30. There are tradeoffs in boiler operation, e.g., as excess air increases, NO_x increases, LOI decreases, and boiler losses increase.

Exhibit 5-29

NO_x vs. LOI Tests–All Sensitivities



The goal is to find and maintain an optimal operating condition. However, what is optimal at full load is not optimal at part load. The I&C systems tested at Plant Hammond included GNOCIS and carbon-in-ash analyzers.

The GNOCIS software applies an optimizing procedure to identify the best set points for the plant, which are implemented automatically without operator intervention (closed-loop), or conveyed to the plant operators for implementation (open-loop). The major elements of GNOCIS are shown in Exhibit 5-31.

SCS has employed GNOCIS in both open-loop advisory and closed-loop supervisory modes. The system has provided advice that reduced NO_x emissions by 10-15% at full load. GNOCIS provided advice that reduced fly ash LOI by 1-3 percentage points and improved boiler efficiency by 0.5 percentage points.

Three carbon-in-ash monitors were installed: Applied Synergistics FOCUS, CAMRAC Corporation CAM, and Clyde-Sturtevant SEKAM. The monitors seemed to represent LOI trends well by responding in the correct direction and provided important and timely information on combustion performance.

Environmental

As shown in Exhibit 5-32, the AOFA, LNBs, and LNB/AOFA provide a long-term full load NO_x reduction of 24, 48, and 68%, respectively. The load-weighted average of NO_x emission reductions was 14, 48, and 63%, respectively, for AOFA, LNB, LNB/AOFA. Although the LNB/AOFA NO_x level represents a 68% reduction from baseline levels, a substantial portion of the incremental change in NO_x emissions between the LNB and the LNB/AOFA configurations is the result of operational changes and is not the result of adding AOFA.

A total of 63 days of valid long-term NO_x emissions data were collected during the LNB/AOFA test phase. Based on this data set, the full-load, long-term NO_x emissions are approximately 0.40 lb/10^6 Btu, which was consistent with earlier short-term test data.

Air toxic testing was conducted for AOFA and LNB/AOFA operation. There was not a significant difference

Exhibit 5-30

Typical Trade-Offs in Boiler Optimization

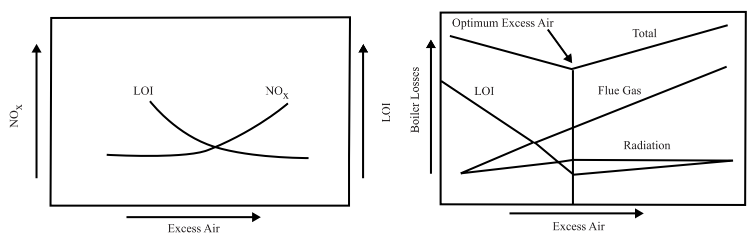
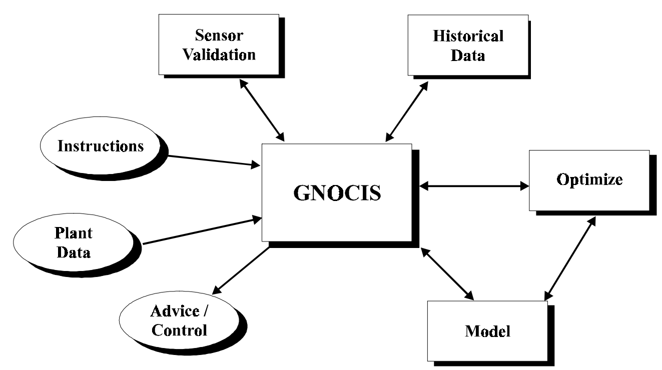


Exhibit 5-31

Major Elements of GNOCIS



in emissions of trace metals, acid gases, and volatile organic compounds for the two tests. There was a slight downward trend, however, in emissions during LNB/AOFA operation. For elements associated with particulate matter, ten (barium, beryllium, chromium, cobalt, copper, lead, manganese, nickel, phosphorus, and vanadium) show lower mean emissions during LNB/AOFA operation; only two (arsenic and cadmium) show higher mean emissions during LNB/AOFA operation. Total particulate matter emissions were also lower during LNB/AOFA operation; however, this was more an indication of ESP performance rather than burner configuration.

Economic

Estimated capital costs for a commercial 500 MWe wall-fired installation are: AOFA—\$8.8/kW, LNB—\$10.0/kW, and GNOCIS—\$0.5/kW. Annual O&M costs and NO_x reductions depend on the assumed load profile. Based on the actual load profile observed in the testing, the estimated annual O&M cost increase for LNB and AOFA is \$333,351. Efficiency is decreased by 1.3 percent, and the NO_x reduction is 68 percent of baseline, or 11,615 tons/year. The capital cost is \$8,300,000 and the calculated cost of NO_x removed is \$86/ton.

The addition of GNOCIS to the same unit, using the actual load profile observed in the testing, results in a range of costs depending on whether the unit is operated to maximize NO_x removal, efficiency, or LOI. For the maximum NO_x removal case, the efficiency is improved by 0.6 percent, the annual O&M cost is decreased by \$228,058, the incremental NO_x reduction is 11 percent (834 tons/year), and the capital cost is \$250,000. The calculated cost per ton of NO_x removed is -\$299.

Commercial Applications

The technology is applicable to the 422 existing pre-NSPS wall-fired boilers in the United States, which burn a variety of coals. The GNOCIS technology is applicable to all fossil fuel-fired boilers, including units fired with natural gas and units co-firing coal and natural gas.

The host has retained the technologies for commercial use. Foster Wheeler has equipped 86 boilers with low-NO_x burner technology (51 domestic and 35 international)—1,800 burners for over 30,000 MWe capacity. Some 19 GNOCIS neural-network control projects are underway and another 17 projects are expected in 1999.

Contacts

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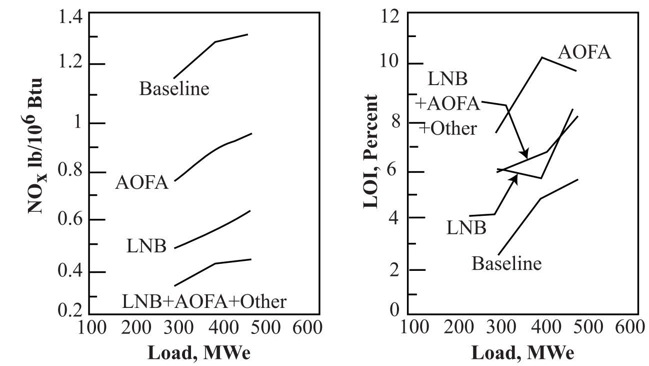
Exhibit 5-32
Performance Test Results



References

- *500 MW Demonstration of Advanced Wall-Fired Combustion Techniques for the Reduction of Nitrogen Oxide (NO_x) Emissions from Coal-Fired Boilers–Public Design Report (Preliminary and Final).* Southern Company Services, Inc. Submitted to DOE on May 24, 1996.
- *500 MW Demonstration of Advanced Wall-Fired Combustion Techniques for the Reduction of Nitrogen Oxide Emissions from Coal-Fired Boilers [Advanced Digital Control/Optimization Phase].* Report No. DOE/PC/89651-T22. Southern Company Services, Inc. January 1995. (Available from NTIS as DE95017742.)
- *500 MW Demonstration of Advanced Wall-Fired Combustion Techniques for the Reduction of Nitrogen Oxide (NO_x) Emissions from Coal-Fired Boilers; Field Chemical Emissions Monitoring; Overfire Air and Overfire Air/Low-NO_x Burner Operation: Final Report.* Report No. DOE/PC/89651-T16. Southern Company Services, Inc. January 1993. (Available from NTIS as DE95006352.)
- *500 MW Demonstration of Advanced Wall-Fired Combustion Techniques for the Reduction of Nitrogen Oxide (NO_x) Emissions from Coal-Fired Boilers–Phase 2 Overfire Air Tests.* Southern Company Services, Inc. and Energy Technology Consultants. Submitted to DOE on August 27, 1992.
- *500 MW Demonstration of Advanced Wall-Fired Combustion Techniques for the Reduction of Nitrogen Oxide (NO_x) Emissions from Coal-Fired Boilers–Phase I Baseline Tests Report.* Southern Company Services, Inc. and Energy Technology Consultants. Submitted to DOE on September 9, 1991.
- *500 MW Demonstration of Advanced Wall-Fired Combustion Techniques for the Reduction of Nitrogen Oxide (NO_x) Emissions from Coal-Fired Boilers–Phases 4—Digital Control System and Optimization.* Southern Company Services, Inc. September 1998.

Environmental Control Devices
Combined SO_2/NO_x
Control Technologies

Milliken Clean Coal Technology Demonstration Project

Project completed.

Participant

New York State Electric & Gas Corporation

Additional Team Members

New York State Energy Research and Development Authority—cofunder

Empire State Electric Energy Research Corporation—cofunder

Consolidation Coal Company—technical consultant

Saarberg-Hölter-Umwelttechnik, GmbH (S-H-U)—technology supplier

The Stebbins Engineering and Manufacturing Company—technology supplier

ABB Air Preheater, Inc.—technology supplier

DHR Technologies, Inc. (DHR)—operator of advisor system

Location

Lansing, Tompkins County, NY (New York State Electric & Gas Corporation's Milliken Station, Unit Nos. 1 and 2)

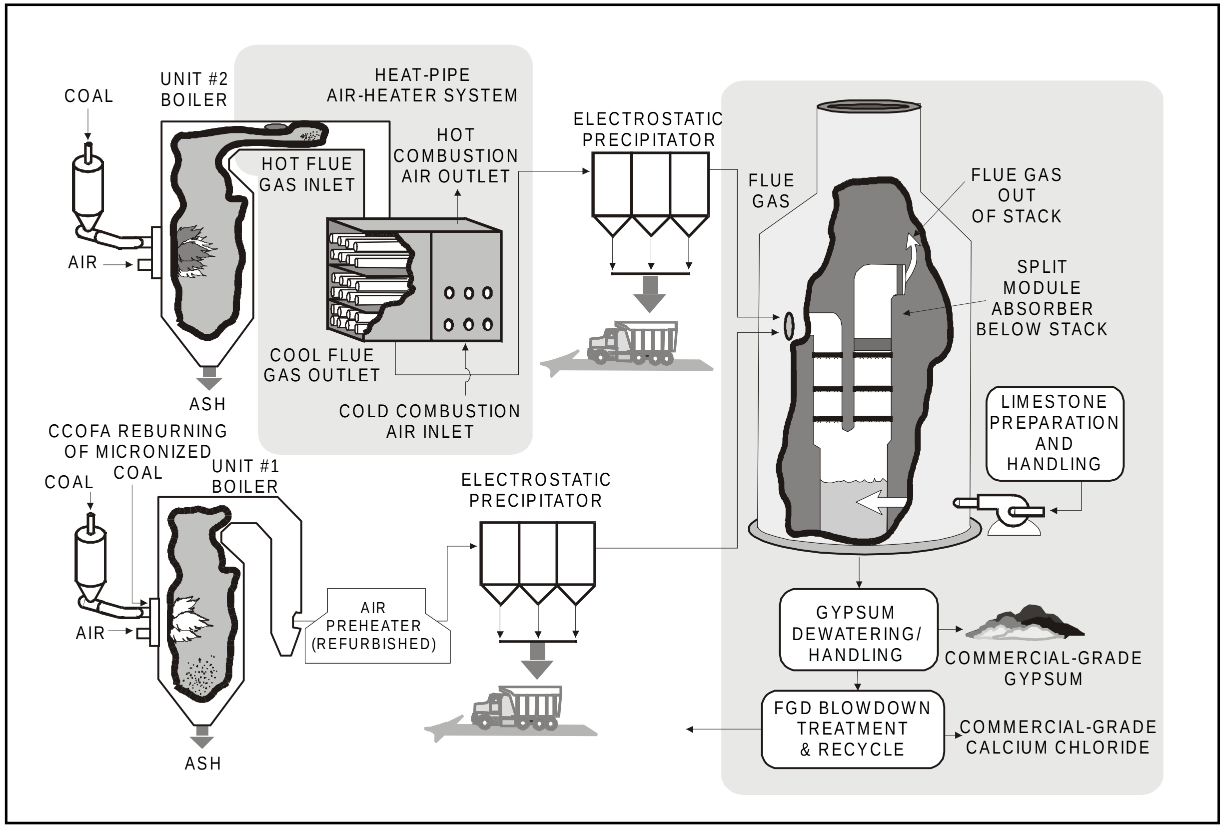
Technology

Flue gas cleanup using S-H-U formic-acid-enhanced, wet limestone scrubber technology; ABB Combustion Engineering's Low-NO_x Concentric Firing System (LNCFS™) Level III; Stebbins' tile-lined split-module absorber; ABB Air Preheater's heat-pipe air preheater; and DHR's PEOA™ Control System.

Plant Capacity/Production

300-MWe

LNCFS is a trademark of ABB Combustion Engineering, Inc.
PEOA is a trademark of DHR Technologies, Inc.



Coals

Pittsburgh, Freeport, and Kittanning Coals; 1.5, 2.9 and 4.0% sulfur, respectively.

Project Funding

Total project cost	$158,607,807	100%
DOE	45,000,000	28
Participant	113,607,807	72

Project Objective

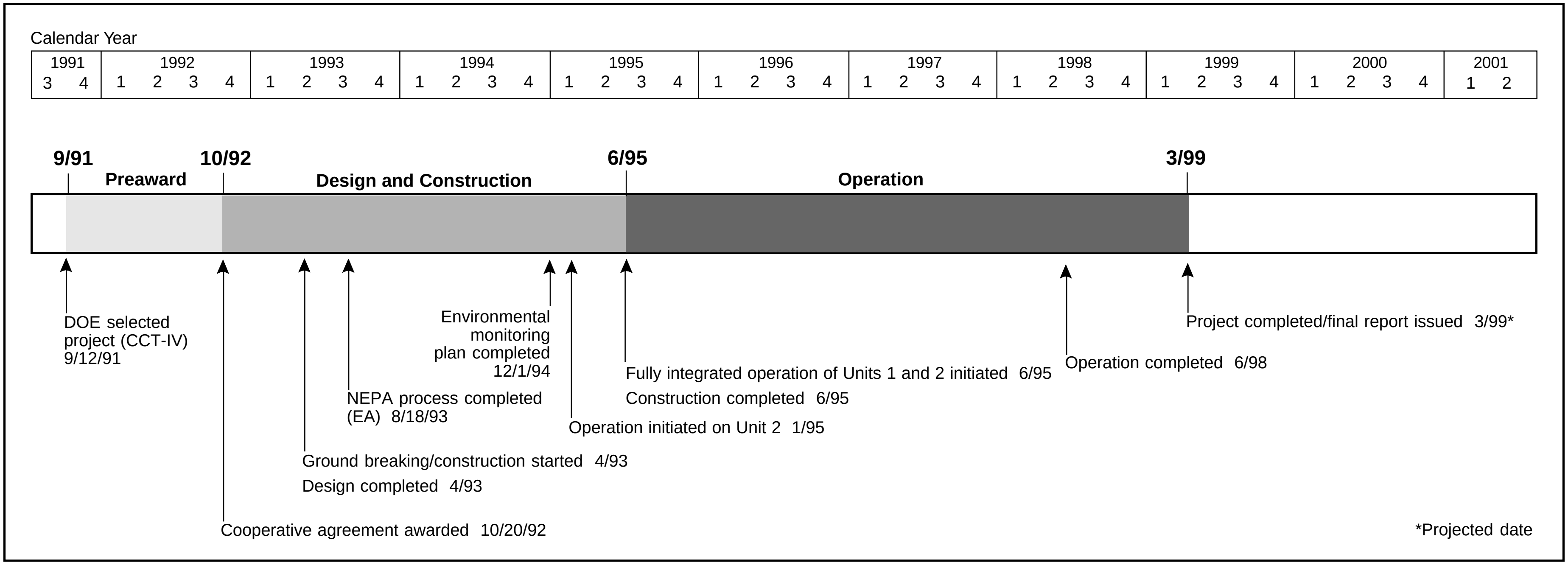
To demonstrate high sulfur capture efficiency and NO_x and particulate control at minimum power requirements, zero waste water discharge, and the production of byproducts in lieu of wastes.

Technology/Project Description

The formic acid enhanced S-H-U process is designed to remove up to 98% SO_2 at high sorbent utilization rates. The Stebbins tile-line, split-module reinforced concrete absorber vessel provides superior corrosion and abrasion resistance. Placement below the stack saves space and provides operational flexibility.

NO_x emissions are controlled by LNCFS III™ low-NO_x burners and by micronized coal reburning. The LNCFS III™ low-NO_x burners are integrated into the Milliken units. See Micronized Coal Reburning Demonstration for NO_x Control for another CCT Program project at this unit.

A heat-pipe air preheater is integrated to increase boiler efficiency by reducing both air leakage and the air preheater's flue gas exit temperature. To enhance boiler efficiency and emissions reductions, DHR's Plant Emission Optimization Advisor (PEOA™) provides state-of-the-art artificial-intelligence-based control of key boiler and plant operating parameters.



Results Summary

Environmental

- The maximum SO_2 removal demonstrated has been 98% with all seven recycle pumps operating and using formic acid. The maximum SO_2 removal without formic acid has been 95%.
- The difference in SO_2 removal between the two limestone grind sizes tested (90%–325 mesh and 90%–170 mesh) while using low sulfur coal was a minimum of 2.6 percentage points.
- The SO_2 removal efficiency was greater than the design during the high velocity test of the cocurrent scrubber section up to a liquid-to-gas ratio of 110.
- The cocurrent pumps had no measurable effect on pressure drop, whereas the countercurrent pumps significantly increased the scrubber pressure drop. The average effect of each countercurrent header was to increase pressure drop by 0.45 inches water column (WC) in the design flow tests and 0.64 inches WC in the high velocity tests.
- Testing of the LNCFS™ III indicated NO_x emissions of 0.39 lb/10^6 Btu (compared to 0.61 lb/10^6 Btu for the original burners).
- During diagnostic tests, LOI was above 4% at full boiler load, during the validation tests (when overfire air limitations were relaxed) the LOI dropped by 0.7 to 1.7 percentage points, with a minor effect on NO_x emissions.
- The NO_xOUT technology at Seward Station successfully demonstrated a 42% reduction NO_x emission reduction from a baseline of 0.78 lb/10^6 Btu to 0.45 lb/10^6 Btu.

Operational

- Performance of the modified ESP exceeded that of the original ESPs at lower power consumption.
- Boiler efficiency was 88.3–88.5% for LNCFS™ III, compared to a baseline of 89.3–89.6%.
- Air filtration is low for both heat pipes. The unaccounted for air leakage rates at full load ranged between 2.0–2.4%.
- The flue gas side pressure loss for both heat pipes was less than the design maximum of 3.65 inches WC. The primary side pressure drops for both heat pipes were less than the design maximum of 3.6 inches WC. The secondary air side pressure drops for both heat pipes were less than the design maximum of 5.35 inches WC.

Economic

- No economic data available.

Project Summary

The test plan was developed to cover all of the new technologies used in the project. In addition to the technologies tested, the project demonstrated that existing technologies can be used in conjunction with new processes to produce saleable by-products. Supplemental monitoring has provided operation and performance data illustrating the success of these processes under a variety of operating conditions. Generally, each test program was divided into four independent subtest: diagnostic, performance, long-term, and validation.

Environmental Performance

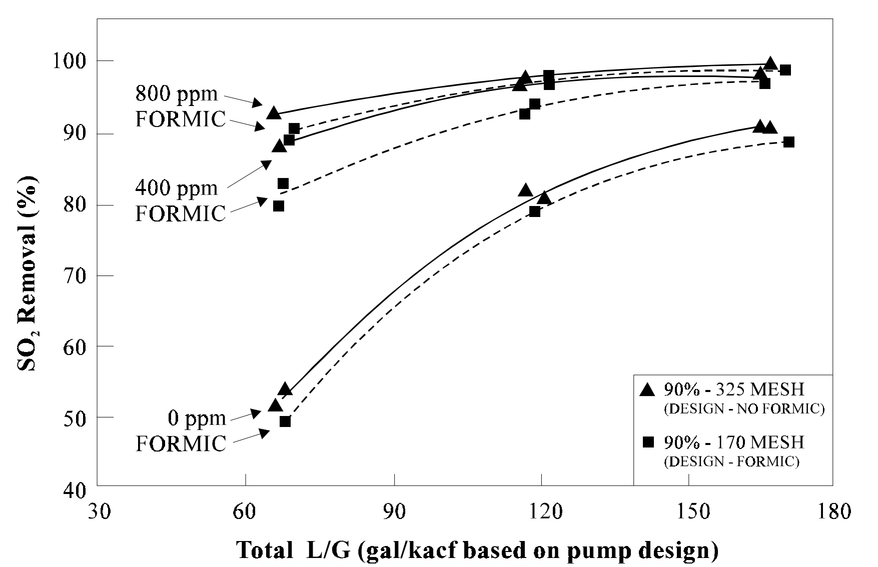
The S-H-U FGD system was tested over a 36 month period. Typical evaluations included SO_2 removal efficiency, power consumption, process economics, load following capability, reagent utilization, by-product quality, and additive effects. Parametric testing included formic acid concentration, L/G ratio, mass transfer, coal sulfur content, and flue gas velocity. Not all test results are currently available. The maximum SO_2 removal demonstrated was 98% with all seven recycle pumps operating and using formic acid and the maximum SO_2 removal without formic acid was 95%. The difference in SO_2 removal between the two limestone grind sizes tested (90%–325 mesh and 90%–170 mesh while using low sulfur coal) was a minimum of 2.6 percentage points as shown in Exhibit 5-33. The SO_2 removal efficiency was greater than the design during the high velocity test of the cocurrent scrubber section up to a liquid-to-gas ratio of 110. The cocurrent pumps had no measurable effect on pressure drop, whereas the countercurrent pumps significantly increased the scrubber pressure drop. As seen in Exhibit 5-34, the average effect of each countercurrent header was to increase pressure drop by 0.45 inches water column (WC) in the design flow tests and 0.64 inches WC in the high velocity tests.

Performance of the modified ESP exceeded that of the original ESPs at lower power consumption. The average penetration before the ESP modification was 0.22% and decreased to 0.12% after the modifications.

At full boiler load (145–150 MWe) and 3.0–3.5% economizer O_2, the LNCFS™ III lowered NO_x emissions from a baseline of .064 lb/10^6 Btu to 0.39 lb/10^6 Btu (39% reduction). At 80-90 MWe boiler load and 4.3–5.0% economizer O_2, the LNCFS™ III lowered NO_x emissions from a baseline of 0.58 lb/10^6 Btu to 0.41 lb/10^6 Btu (29% reduction). With LNCFS™ III, LOI was maintained below 4% and CO emissions did not increase.

Exhibit 5-33

Effect of Limestone Grind



Operational Performance

The S-H-U FGD system performance goal of 98% SO_2 removal efficiency was achieved. Similarly, the objective of producing a marketable gypsum by-product from the FGD system was achieved. The test results indicate the gypsum produced can be maintained at a purity level exceeding 95% with a chloride level less than 100 ppm. However, the goal of producing a marketable calcium chloride solution from the FGD blowdown stream was not achieved. FGD availability for the test period was 99.9%.

The modified ESP performed better than the original ESP at a lower power use. The total voltage•current product (V•I) for ESPs is directly proportional to the total power requirement. The modified ESP 75% of the V•I demand of the original ESPs. The modified ESP has a smaller plant footprint with fewer internals and a smaller SCA. Total internal plate area is less than one-half that of the original ESPs, tending to lower capital costs.

Boiler efficiency was 88.3–88.5% for LNCFS™ III, compared to a baseline of 89.3–89.6%. The lower efficiency was attributed to higher post retrofit flue gas O_2 and higher stack temperatures which accompanied the air heater retrofit. When LNCFS™ III and baseline conditions are compared, boiler efficiency with LNCFS™ III was 0.2 percentage points higher than baseline.

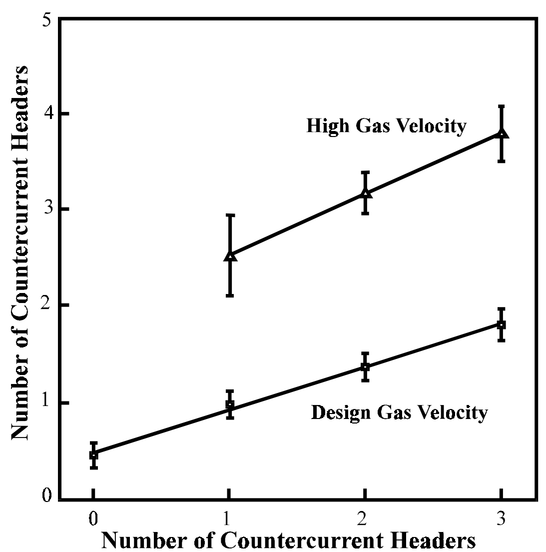
The heat pipe were tested in accordance with ASME Power test Code for Air Heaters 4.3. Air filtration is low for both heat pipes. The unaccounted for air leakage rates at full load ranged between 2.0–2.4%. The tests showed that the flue gas side pressure loss for both heat pipes was less than the design maximum of 3.65 inches WC. The primary side pressure drops for both heat pipes were less than the design maximum of 3.6 inches WC. The secondary air side pressure drops for both heat pipes were less than the design maximum of 5.35 inches WC.

The main problem with the NO_xOUT technology was with ammonia slip, which is a byproduct of the urea injected into the boiler. The ammonia reacts with sulfur trioxide in the flue gas to form ammonium bisulfate in the air heaters. If the ammonia slip is not consistently maintained below 2 ppm significant pluggage of the air heater can result in a short period of time.

Economic Performance

Economic data is not yet available.

Exhibit 5-34
Pressure Drop vs. Countercurrent Headers



Commercial Applications

The S-H-U process, stebbins absorber module, NO_xOUT® system, and heat-pipe air preheater are applicable to virtually all power plants. The space-saving design features of the technologies, combined with the production of marketable byproducts, offer significant incentives to generating stations with limited space.

There have been four commercial sales of the PEOA™ system. Commercial sales of the NO_xOUT® system have been made to at least a dozen companies and a licensing agreement has been signed with Wheelabrator. More than 20 units have been sold in the United States, Taiwan, and Korea. Several of these sales are for a derivative reduction system. Applications span industrial and utility boilers, municipal solid waste incinerators, wood-waste-fired furnaces, and steel production.

Contacts

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James U. Watts, FETC, (412) 892-5991

References

- *Comprehensive Report to Congress on the Clean Coal Technology Program: Milliken coal Technology Demonstration Project.* New York State Electric & Gas Corporation. Report No. DOE/FE-0265P. U.S. Department of Energy. September 1992. (Available from NTIS as DE93001756.)
- *Milliken Clean Coal Technology Demonstration Project.* Harvilla, James et al. *Sixth Clean Coal Technology Conference: Clean Coal for the 21st Century — What Will It Take? Volume II - Technical Papers.* CONF-980410— VOL II. April 28-May 1, 1998.

Commercial Demonstration of the NOXSO SO_2/NO_x Removal Flue Gas Cleanup System

Participant
NOXSO Corporation

Additional Team Members
Olin Corporation—cofunder
Gas Research Institute—cofunder
Electric Power Research Institute—cofunder
W.R. Grace and Company—cofunder
Morrison Knudsen-Ferguson—engineer
Richmond Power & Light (RP&L)—host

Location
Not applicable

Technology
NOXSO Corporation's dry, regenerable flue gas cleanup process

Plant Capacity/Production
Not applicable

Coal
Medium- to high-sulfur coals

Project Funding

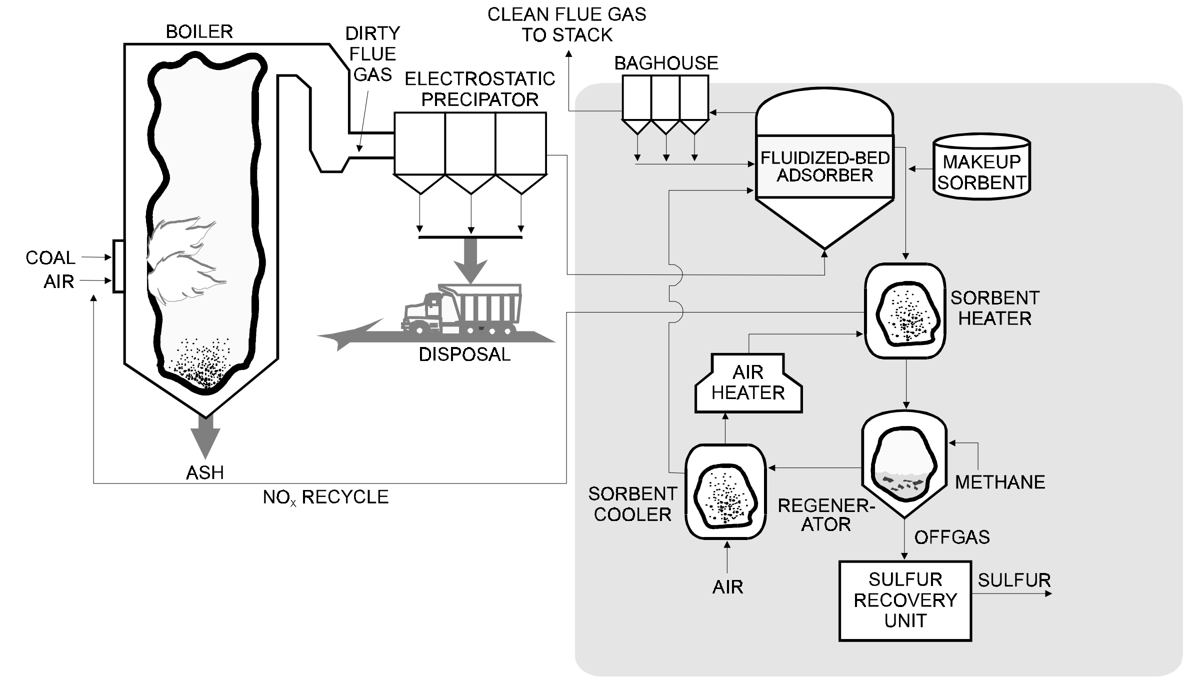
Total project cost	$82,812,120	100%
DOE	41,406,060	50
Participant	41,406,060	50

Project Objective
To demonstrate removal of 98% of the SO_2 and 75% of the NO_x from a coal-fired boiler's flue gas using the NOXSO process.

Technology/Project Description
The NOXSO process is a dry, regenerable system capable of removing both SO_2 and NO_x in flue gas from coal-fired utility boilers burning medium- to high-sulfur coals. In the basic process, the flue gas passes through a fluidized-bed adsorber located downstream of the precipitator; SO_2 and NO_x are adsorbed by the sorbent, which consists of spherical beads of high-surface-area alumina impregnated with sodium carbonate. Cleaned flue gas then passes through a baghouse to the stack.

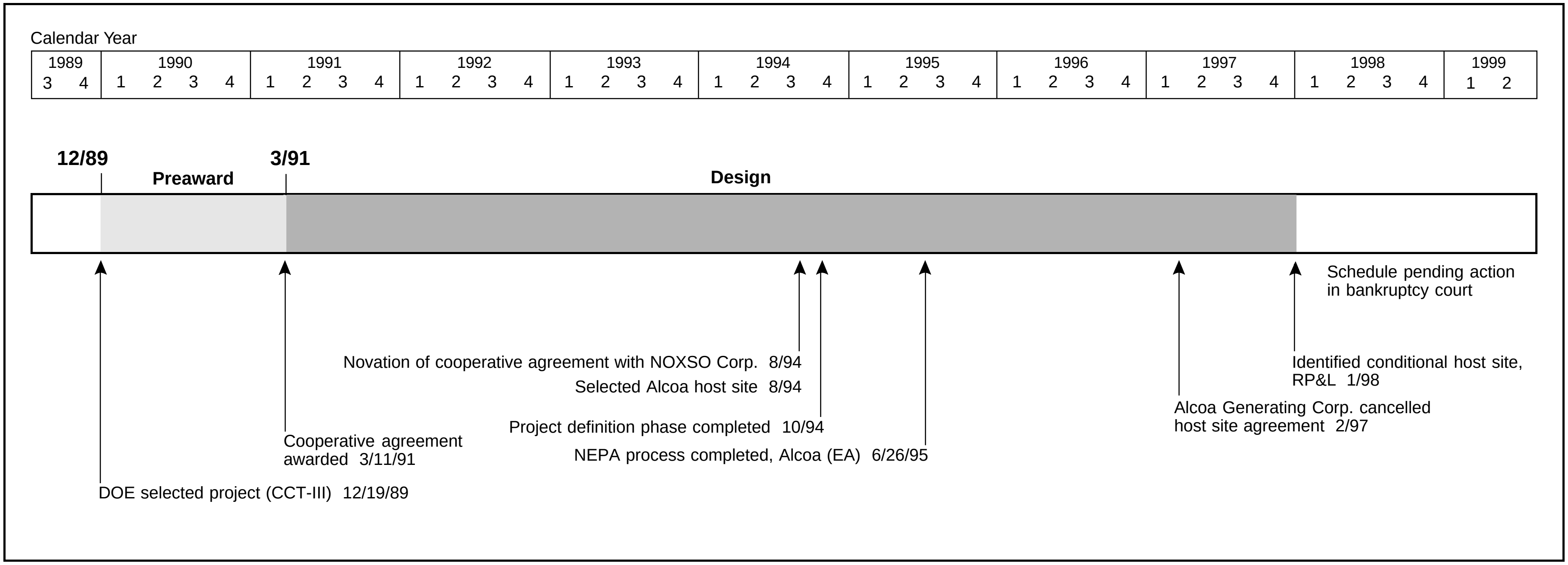
The NO_x is desorbed from the NOXSO sorbent when heated by a stream of hot air. Hot air containing the desorbed NO_x is recycled to the boiler where equilibrium processes cause destruction of the NO_x. The adsorbed sulfur is recovered from the sorbent in a regenerator where it reacts with methane at high temperature to produce an offgas with high concentrations of SO_2 and hydrogen sulfide (H_2S). This offgas is processed to produce elemental sulfur, which can be further processed to produce liquid SO_2, a higher valued by-product.

The process is expected to achieve SO_2 reductions of 98% and NO_x reductions of 75%.



Project Status/Accomplishments
Alcoa Generating Corporation chose to cancel the host site agreement when NOXSO was unable to obtain full project financing by January 31, 1997, as specified in the agreement. NOXSO signed a conditional Host Site Agreement with RP&L in January 1998.

On September 22, 1998 NOXSO issued a press release stating that they have requested the bankruptcy court to change their filing from a Chapter 11 - Reorganization to Chapter 7 - Liquidation. This change was prompted by an inability to raise funding for their cost



share of a continued project. However, the unsecured creditor committee requested the court keep NOXSO in Chapter 11.

Commercial Applications

The NOXSO process is applicable for retrofit or new facilities. The process is suitable for utility and industrial coal-fired boilers. The process is adaptable to coals with medium- to high-sulfur content.

The process produces one of the following as a salable by-product: elemental sulfur, sulfuric acid, or liquid SO_2. A readily available market exists for these products.

The technology is expected to be especially attractive to utilities that require high removal efficiencies for both SO_2 and NO_x, need to eliminate solid wastes, and/or have inadequate water supply for a wet scrubber.

SNOX™ Flue Gas Cleaning Demonstration Project

Project completed.

Participant
ABB Environmental Systems

Additional Team Members
Ohio Coal Development Office—cofunder
Ohio Edison Company—cofunder and host
Haldor Topsoe a/s—patent owner for process technology, catalysts, and WSA Tower
Snamprogetti, U.S.A.—cofunder and process designer

Location
Niles, Trumbull County, OH (Ohio Edison's Niles Station, Unit No. 2)

Technology
Haldor Topsoe's SNOX™ catalytic advanced flue gas cleanup system

Plant Capacity/Production
35-MWe equivalent slipstream from a 108-MWe boiler

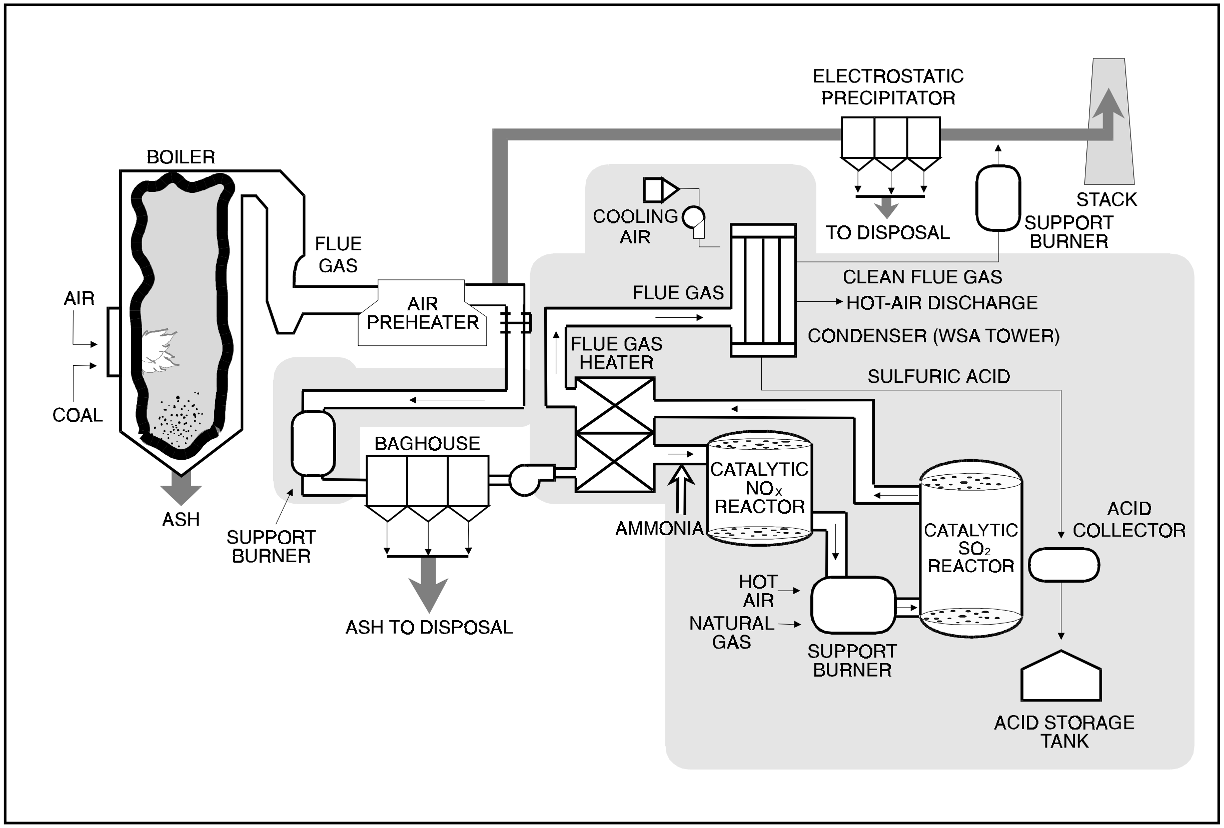
Coal
Ohio bituminous, 3.4% sulfur

Project Funding

Total project cost	$31,438,408	100%
DOE	15,719,200	50
Participant	15,719,208	50

Project Objective
To demonstrate at an electric power plant using U.S. coals that SNOX™ technology will catalytically remove 95% of SO_2 and more than 90% of NO_x from flue gas and produce a salable by-product of concentrated sulfuric acid.

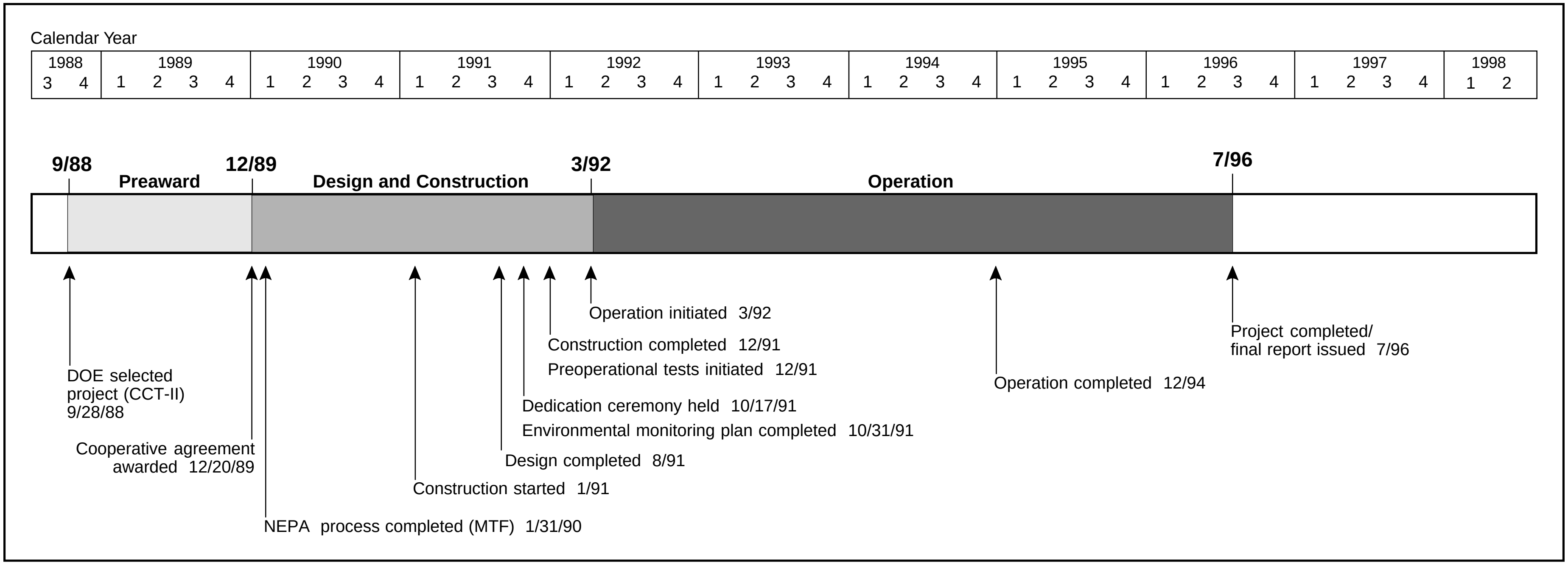
SNOX is a trademark of Haldor Topsoe a/s.



Technology/Project Description
In the SNOX™ process, the stack gas leaving the boiler is cleaned of fly ash in a high-efficiency fabric filter baghouse to minimize the cleaning frequency of the sulfuric acid catalyst in the downstream SO_2 converter. The ash-free gas is reheated, and NO_x is reacted with small quantities of ammonia in the first of two catalytic reactors where the NO_x is converted to harmless nitrogen and water vapor. The SO_2 is oxidized to SO_3 in a second catalytic converter. The gas then passes through a novel glass-tube condenser that allows SO_3 to hydrolyze to concentrated sulfuric acid.

The technology, while using U.S. coals, was designed to remove 95% of the SO_2 and more than 90% of the NO_x from flue gas and produce a salable sulfuric acid by-product. This was accomplished without using sorbents and without creating waste by-products.

The demonstration was conducted at Ohio Edison's Niles Station in Niles, OH. The demonstration unit treated a 35-MWe equivalent slipstream of flue gas from the 108-MWe Unit No. 2 boiler, which burned a 3.4% sulfur Ohio coal. The process steps were virtually the same as for a commercial full-scale plant, and commercial-scale components were installed and operated.



Results Summary

Environmental

- SO_2 removal efficiency was normally in excess of 95% for inlet concentrations averaging about 2,000 ppm.
- NO_x reduction averaged 94% for inlet concentrations of approximately 500–700 ppm.
- Particulate removal efficiency for the high-efficiency fabric filter baghouse with SNOX™ system was greater than 99%.
- Sulfuric acid purity exceeded federal specifications for Class I acid.
- Air toxics testing showed high capture efficiency of most trace elements in the baghouse. A significant portion of the boron and almost all of the mercury escaped to the stack. But selenium and cadmium, normally a problem, were effectively captured in the acid drain, as were organic compounds.
- Absence of an alkali reagent contributed to having no secondary pollution streams or increases in CO_2 emissions.
- SO_2 catalyst virtually eliminated CO and hydrocarbon emissions.

Operational

- SO_2 catalyst downstream of the NO_x catalyst eliminated ammonia slip and allowed the SCR to function more efficiently.
- Heat developed in the SNOX™ process was used to enhance thermal efficiency.

Economic

- Capital cost was estimated at $305/kW for a 500-MWe unit firing 3.2% sulfur coal. The levelized incremental cost was estimated at 6.1 mills/kWh or $219/ton of SO_2 removal on a constant dollar basis. Comparable current dollar costs were 7.8 mills/kWh and $284/ton of SO_2.

Project Summary

Because the SNOX™ process utilized an oxidation catalyst to convert SO_2 to SO_3 and ultimately to sulfuric acid, no reagent was required for the SO_2 removal step. As a result, the process produced no other waste streams.

In order to demonstrate and evaluate the performance of the SNOX™ process, general operating data were collected and parametric tests conducted to characterize the process and equipment. The system has operated for approximately 8,000 hours and produced more than 5,600 tons of commercial-grade sulfuric acid. Many tests for the SNOX™ system were conducted at three loads—75, 100, and 110% of design capacity.

Environmental Performance

Particulate emissions from the process were very low (<1 mg/Nm^3) due to the characteristics of the SO_2 catalyst and the sulfuric acid condenser (WSA Condenser). Although the Niles SNOX™ plant was fitted with a baghouse (rather than an ESP) on its inlet, this was not necessary for low particulate emissions, but the baghouse was needed to maintain an acceptable cleaning frequency of the SO_2 catalyst. At operating temperature, the SO_2 catalyst, because of its sticky surface, retained about 90% of the dust that entered the catalyst vessel. Dust that passed through was subsequently removed in the WSA Condenser, which acted as a condensing particulate removal device (utilizing the dust particulates as nuclei).

Minimal or no increase in CO_2 emissions by the process was tied to two features—the lack of a carbonate-based alkali reagent that releases CO_2 and the fact that the process recovered additional heat from the flue gas to offset its parasitic energy requirements. This heat recovery, under most design conditions, results in the net heat rate of the boiler being the same or better after addition of the SNOX™ process, and consequently no increase in CO_2 generation per unit of power.

With respect to CO and hydrocarbons, the SO_2 catalyst acted to virtually eliminate these compounds as well. This aspect also positively affected the interaction of the NO_x and SO_2 catalysts. Because the SO_2 catalyst followed the NO_x catalyst, any unreacted ammonia (slip) was oxidized in the SO_2 catalyst to nitrogen, water vapor, and a small amount of NO_x. As a result, downstream fouling by ammonia compounds was eliminated and the SCR was operated at slightly higher than typical ammonia stoichiometries. These higher stoichiometries allowed smaller SCR catalyst volumes and permitted the attainment of very high reduction efficiencies (>95%).

Sulfur dioxide removal in the SNOX™ process was controlled by the efficiency of the SO_2-to-SO_3 oxidation, which occurred as the flue gas passes through the oxidation catalyst beds. The efficiency was controlled by two factors—space velocity and bed temperature. Space velocity governed the amount of catalyst necessary at design flue gas flow conditions, and gas and bed temperature had to be high enough to activate the SO_2 oxidation, reaction. During the test program, SO_2 removal efficiency was normally in excess of 95% for inlet concentrations averaging about 2,000 ppm.

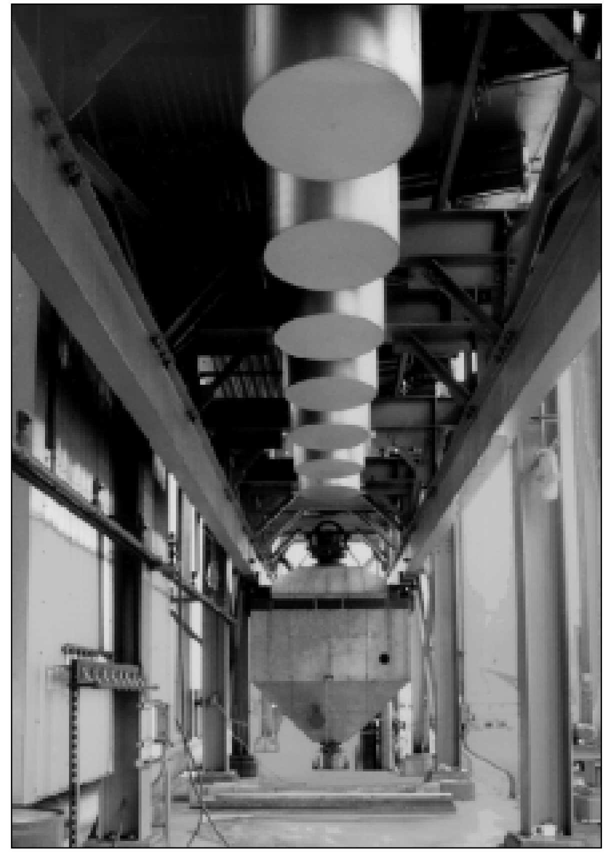
The SCR portion of the SNOX™ process was able to operate at higher than typical ammonia stoichiometries due to its location ahead of the SO_2 catalyst beds. Normal operating stoichiometries for the SCR system were in the range of 1.02–1.05 and system reduction efficiencies averaged 94% with inlet NO_x levels of approximately 500–700 ppm.

Sulfuric acid concentration and composition has met or exceeded the requirements of the federal specifications for Class I acid. During the design and construction of the SNOX™ demonstration, arrangements were made with a sulfuric acid supplier to purchase and distribute the acid from the plant. The acid has been sold to the agriculture industry for the production of diammonium phosphate fertilizer and to the steel industry for pickling. Ohio Edison has also used a significant amount in boiler water demineralizer systems throughout its plants.

Air toxic testing conducted at the Niles SNOX™ plant measured the following substances:

- Five major and 16 trace elements including mercury, chromium, cadmium, lead, selenium, arsenic, beryllium, and nickel
- Acids and corresponding anions (hydrogen chloride, hydrogen fluoride, chloride, fluoride, phosphate, sulfate)
- Ammonia and cyanide
- Elemental carbon
- Radionuclides
- Volatile organic compounds
- Semi-volatile compounds including polynuclear aromatic hydrocarbons
- Aldehydes

Most trace elements were captured in the baghouse along with the particulate. A significant portion of the boron and almost all of the mercury escaped to the stack.



▲ The bottom portion of the SO_2 converter catalyst, with the catalyst dust collector hopper mounted on steel rails (center), is shown.

But selenium and cadmium, normally a problem, were effectively captured in the acid drain, as were organic compounds.

Operational Performance

Heat recovery was accomplished by the SNOX™ process. In a commercial configuration, it can be utilized in the thermal cycle of the boiler. The process generated recoverable heat in several ways. All of the reactions that took place with respect to NO_x and SO_2 removal were exothermic and increased the temperature of the flue gas. This heat plus fuel-fired support heat added in the high-temperature SCR/SO_2 catalyst loop was recovered in the WSA Condenser cooling air discharge for use in the furnace as combustion air. Because the WSA Condenser lowered the temperature of the flue gas to about 210 ºF, compared to approximately 300 ºF for a typical power plant, additional thermal energy was recovered along with that from the heats of reaction.

Economic Performance

The economic evaluation of the SNOX™ process showed a capital cost of approximately $305/kW for a 500-MWe unit firing 3.2% sulfur coal. The levelized incremental cost was 6.1 mills/kWh on a constant dollar basis and 7.8 mills/kWh on a current dollar basis. The equivalent costs per ton of SO_2 removed were $219/ton (constant 1995 dollars) and $384 (current dollars).

Commercial Applications

The SNOX™ technology is applicable to all electric power plants and industrial/institutional boilers firing coal, oil, or gas. The high removal efficiency for NO_x and SO_2 makes the process attractive in many applications. Elimination of additional solid waste (except ash) enhances the marketability in urban and other areas where solid waste disposal is a significant problem.

The host utility, Ohio Edison, is retaining the SNOX™ technology as a permanent part of the pollution control system at Niles Station to help Ohio Edison meet its overall SO_2/NO_x reduction goals.

Commercial SNOX™ plants also are operating in Denmark and Sicily. In Denmark, a 305-MWe plant has operated since August 1991. The boiler at this plant burns coals from various suppliers around the world, including the United States; the coals contain 0.5–3.0% sulfur. The plant in Sicily, operating since March 1991, has a capacity of about 30-MWe and fires petroleum coke.

◄ The SNOX™ demonstration at Ohio Edison's Niles Station Unit No. 2 achieved SO_2 removal efficiencies exceeding 95% and NO_x reduction effectiveness averaging 94%. Ohio Edison is retaining the SNOX™ technology as part of its environmental control system.

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References

- *Final Report Volume II: Project Performance and Economics.* July 1996. Report No. DE-FC22-90PC89C55.
- *Final Report Volume I: Public Design*. Report No. DOE/PC/89655-T21. (Available from NTIS as DE96050312.)
- *A Study of Toxic Emissions from a Coal-Fired Power Plant Utilizing the SNOX™ Innovative Clean Coal Technology Demonstration. Volume 1, Sampling/Results/Special Topics: Final Report.* Report No. DOE/PC/93251-T3-Vol. 1. Battelle Columbus Operations. July 1994. (Available from NTIS as DE94018832.)
- *A Study of Toxic Emissions from a Coal-Fired Power Plant Utilizing the SNOX™ Innovative Clean Coal Technology Demonstration. Volume 2, Appendices: Final Report.* Report No. DOE/PC/93251-T3-Vol. 2. Battelle Columbus Operations. July 1994. (Available from NTIS as DE94018833.)
- *Comprehensive Report to Congress on the Clean Coal Technology Program: WSA-SNOX™ Flue Gas Cleaning Demonstration Project.* ABB Combustion Engineering, Inc. Report No. DOE/FE-0151. U.S. Department of Energy. November 1989. (Available from NTIS as DE90004461.)

LIMB Demonstration Project Extension and Coolside Demonstration

Project completed.

Participant
The Babcock & Wilcox Company

Additional Team Members
Ohio Coal Development Office—cofunder
Consolidation Coal Company—cofunder and technology supplier
Ohio Edison Company—host

Location
Lorain, Lorain County, OH (Ohio Edison's Edgewater Station, Unit No. 4)

Technology
The Babcock & Wilcox Company's (B&W) limestone injection multistage burner (LIMB) system; Babcock & Wilcox DRB-XCL® low-NO_x burners
Consolidation Coal Company's Coolside duct injection of lime sorbents

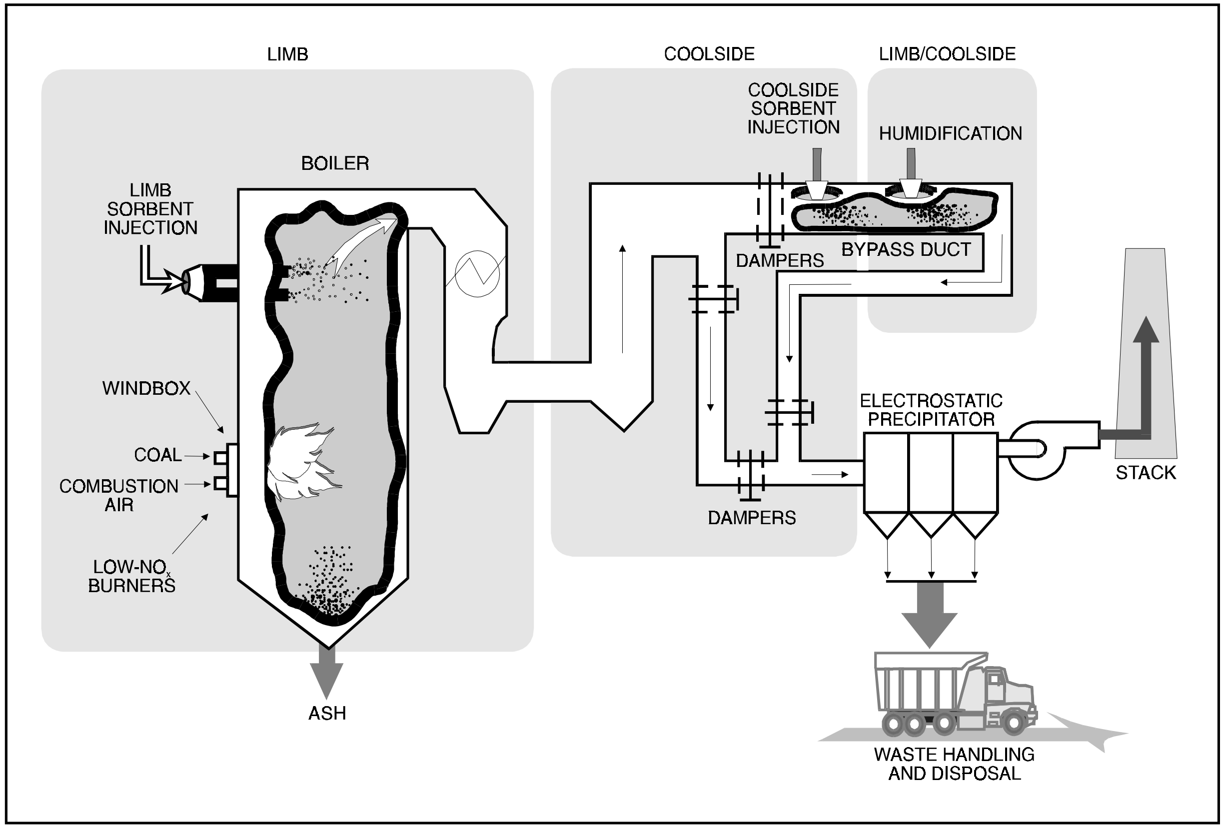
Plant Capacity/Production
105-MWe

Coal
Ohio bituminous, 1.6, 3.0, and 3.8% sulfur

Project Funding

Total project cost	$19,404,940	100%
DOE	7,597,026	39
Participant	11,807,914	61

DRB-XCL is a registered trademark of The Babcock & Wilcox Company.
TAG is a trademark of the Electric Power Research Institute.

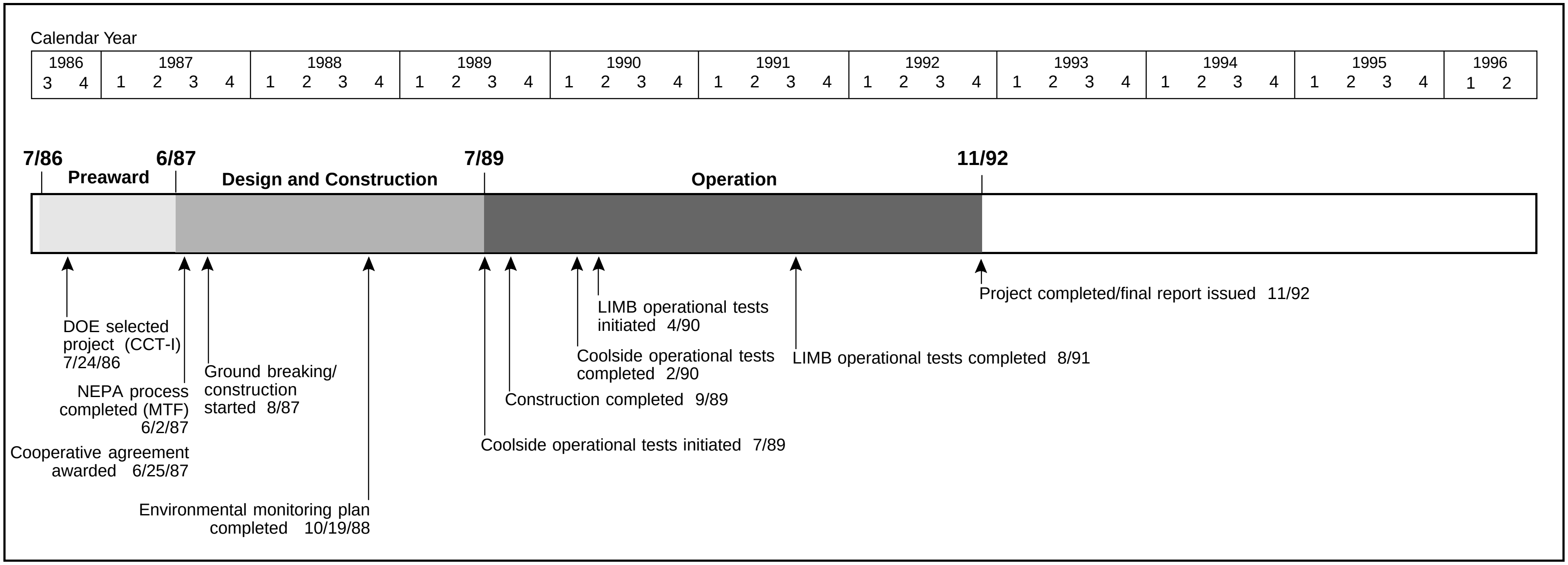


Project Objective
To demonstrate, with a variety of coals and sorbents, the LIMB process as a retrofit system for simultaneous control of NO_x and SO_2 in the combustion process, and that LIMB can achieve up to 70% NO_x and SO_2 reductions; to test alternate sorbent and coal combinations using the Coolside process; to demonstrate in-duct sorbent injection upstream of the humidifier and precipitator; and to show SO_2 removal of up to 70%.

Technology/Project Description
The LIMB process reduces SO_2 by injecting dry sorbent into the boiler at a point above the burners. The sorbent then travels through the boiler and is removed along with fly ash in an electrostatic precipitator (ESP) or baghouse. Humidification of the flue gas before it enters an ESP is necessary to maintain normal ESP operation and to enhance SO_2 removal. Combinations of three bituminous coals (1.6, 3.0, and 3.8% sulfur) and four sorbents were tested. Other variables examined were stoichiometry, humidifier outlet temperature, and injection level.

In the Coolside process, dry sorbent is injected into the flue gas downstream of the air preheater, followed by flue gas humidification. Humidification enhances ESP performance and SO_2 absorption. SO_2 absorption is improved by dissolving NaOH or Na_2CO_3 in the humidifica-tion water. The spent sorbent is collected with the fly ash, as in the LIMB process. Bituminous coal with 3.0% sulfur was used in testing.

Babcock & Wilcox DRB-XCL® low-NO_x burners, which control NO_x through staged combustion, were used in demonstrating both LIMB and Coolside technologies.



Results Summary

Environmental

- LIMB SO_2 removal efficiencies at a calcium-to-sulfur (Ca/S) molar ratio of 2.0 and minimal humidification across the range of coal sulfur contents were 53–61% for ligno lime, 51–58% for calcitic lime, 45–52% for dolomitic lime, and 22–25% for limestone ground to 80% less than 44 microns (325 mesh).
- LIMB SO_2 removal efficiency increased to 32% using limestone ground to 100% minus 325 mesh and increased an additional 5–7% when ground to 100% less than 10 microns.
- LIMB SO_2 removal efficiencies were enhanced by about 10% when humidification down to 20 ºF approach-to-saturation temperature was used.
- LIMB, which incorporated Babcock & Wilcox DRB-XCL® low-NO_x burners, achieved 40–50% NO_x reduction.
- Coolside SO_2 removal efficiency was 70% at a Ca/S molar ratio of 2.0, a sodium-to-calcium (Na/Ca) ratio of 0.2, and 20 ºF approach-to-adiabatic-saturation temperature using commercial hydrated lime and 2.8–3.0% sulfur coal.
- Sorbent recycle tests demonstrated the potential to improve sorbent utilization.

Operational

- Humidification enhanced ESP performance, which enabled opacity levels to be kept well within limits.
- LIMB availability was 95%. Coolside did not undergo testing of sufficient length to establish availability.
- Humidifier performance indicated that operation in a vertical rather than horizontal mode would be better.

Economic

- LIMB capital costs were \$31–102/kW for plants 100–500-MWe and coals with 1.5–3.5% sulfur, with a target SO_2 reduction of 60% (1992 \$). Annual levelized costs (15-year) for this range of conditions were \$392–791/ton of SO_2 removed.
- Coolside capital costs were \$69–160/kW for plants 100–500-MWe and coals with 1.5–3.5% sulfur, with a target SO_2 reduction of 70% (1992 \$). Annualized levelized costs (15-year) for this range of conditions were \$482–943/ton of SO_2 removed.

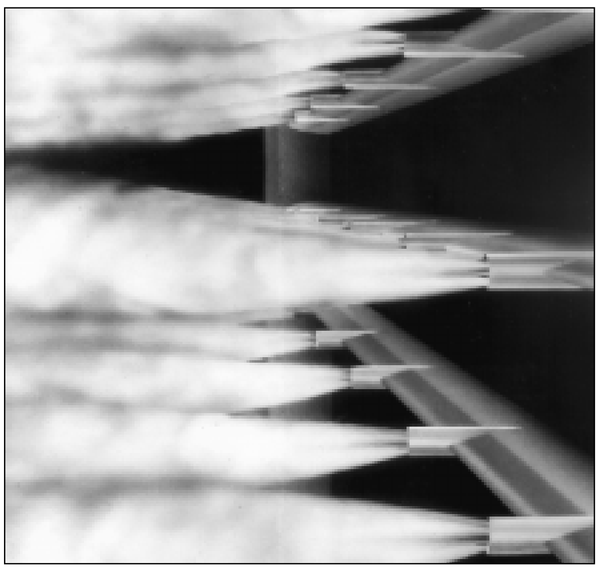
Project Summary

The initial expectation with LIMB technology was that limestone calcined by injection into the furnace would achieve adequate SO_2 capture. Use of limestone in lieu of the significantly more expensive lime would keep operating costs relatively low. However, the demonstration showed that even with fine grinding of the limestone and deep humidification, performance with limestone was marginal. As a result, a variety of hydrated limes were evaluated in the LIMB configuration, demonstrating enhanced performance. Although LIMB performance was enhanced by applying humidification to the point of approaching adiabatic saturation temperatures, performance did not rely on this deep humidification.

Coolside design was dependent upon deep humidification to improve sorbent reactivity and use of hydrated lime. Sorbent injection was downstream of the furnace. In addition, sorbent activity was enhanced by dissolving sodium hydroxide (NaOH) or sodium carbonate (Na_2CO_3) in the humidification water.

Environmental Performance (LIMB)

LIMB tests were conducted over a range of Ca/S molar ratio and humidification conditions while burning Ohio coals with nominal sulfur contents of 1.6, 3.0, and 3.8% by weight. Each of four different sorbents was injected while burning each of the three different coals. Other variables examined were stoichiometry, humidifier outlet temperature, and injection level. Exhibit 5-35 summarizes SO_2 removal efficiencies for the range of sorbents and coals tested.



▲ Water mist, sprayed into the flue gas, enhanced sulfur capture by the sorbent by approximately 10% in the LIMB process when 20 ºF approach-to-saturation was used.

While injecting commercial limestone with 80% of the particles less than 44 microns in size, removal efficiencies of about 22% were obtained at a stoichiometry of 2.0 while burning 1.6% sulfur coal. However, removal efficiencies of about 32% were achieved at a stoichiometry of 2.0 when using a limestone with a smaller particle size (i.e., all particles were less than 44 microns). A third limestone with essentially all particles less than 10 microns was used to determine what might be the removal efficiency limit. The removal efficiency for this very fine limestone was approximately 5–7% higher than that obtained at similar conditions for limestone with particles all sized less than 44 microns.

During the design phase, it was expected that injection at the 181-feet plant elevation level inside the boiler would permit the introduction of the limestone at close to the optimum furnace temperature of 2,300 ºF. Testing confirmed that injection at this level, just above the nose of the boiler, yielded the highest SO_2 removal. Injection was also performed at the 187-feet level and similar removals were observed. Removal efficiencies while injecting at these levels were about 5% higher than while injecting sorbent at the 191-feet level.

Removal efficiencies were enhanced by approximately 10% over the range of stoichiometries tested when humidification down to a 20 ºF approach-to-saturation temperature was used.

The continued use of the low-NO_x burners resulted in an overall average NO_x emissions level of 0.43 lb/10^6 Btu, which is about a 45% reduction.

Operational Performance (LIMB)

Long-term test data showed that the LIMB system was available about 95% of the time it was called upon to operate. Even with minimal humidification, ESP performance was adequately enhanced to keep opacity levels well below the permitted limit. Opacity was generally in the 2–5% range while the limit was 20%.

Exhibit 5-35
LIMB SO_2 Removal Efficiencies
(Percent)

Sorbent	Nominal Coal Sulfur Content 3.8%	3.0%	1.6%
Ligno lime	61	63	53
Commercial calcitic lime	58	55	51
Dolomitic lime	52	48	45
Limestone (80% <44 microns)	NT	25	22

NT = Not tested
Test conditions: injection at 181 ft, Ca/S molar ratio of 2.0, minimal humidification.

Environmental Performance (Coolside)

The Coolside process was tested while burning compliance (1.2–1.6% sulfur) and noncompliance (2.8–3.2% sulfur) coals. Objectives of the full-scale test program were to verify short-term process operability and to develop a design performance database to establish process economics for Coolside. Key process variables—Ca/S molar ratio, Na/Ca molar ratio, and approach-to-adiabatic-saturation—were evaluated in short-term (6–8-hour) parametric tests and longer term (1–11-day) process operability tests.

The test program demonstrated that the Coolside process routinely achieved 70% SO_2 removal at design conditions of 2.0 Ca/S molar ratio, 0.2 Na/Ca molar ratio, and 20 ºF approach-to-adiabatic-saturation temperature using commercially available hydrated lime. Coolside SO_2 removal depended on Ca/S molar ratio, Na/Ca molar ratio, approach-to-adiabatic-saturation, and the physical properties of the hydrated lime. Sorbent recycle showed significant potential to improve sorbent utilization. The observed SO_2 removal with recycled sorbent alone was

Exhibit 5-36
Capital Cost Comparison
(1992 $/kW)

Coal (%S)	LIMB	Coolside	LSFO	LIMB	Coolside	LSFO
	100-MWe			**150-MWe**		
1.5	93	150	413	66	116	312
2.5	95	154	421	71	122	316
3.5	102	160	425	73	127	324
	250-MWe			**500-MWe**		
1.5	46	96	228	31	69	163
2.5	50	101	235	36	76	169
3.5	54	105	240	40	81	174

Exhibit 5-37
Annual Levelized Cost Comparison
(1992 $/Ton of SO_2 Removed)

Coal (%S)	LIMB	Coolside	LSFO	LIMB	Coolside	LSFO
	100-MWe			**150-MWe**		
1.5	791	943	1418	653	797	1098
2.5	595	706	895	520	624	692
3.5	525	629	665	461	570	527
	250-MWe			**500-MWe**		
1.5	549	704	831	480	589	623
2.5	456	567	539	416	502	411
3.5	419	526	413	392	482	321

22% at 0.5 available Ca/S molar ratio and 18 ºF approach-to-adiabatic-saturation. The observed SO_2 removal with simultaneous recycle and fresh sorbent feed was 40% at 0.8 fresh Ca/S molar ratio, 0.2 fresh Na/Ca molar ratio, 0.5 available recycle, and 18 ºF approach-to-adiabatic-saturation.

Operational Performance (Coolside)

Floor deposits experienced in the ductwork with the horizontal humidification led designers to consider a vertical unit in a commercial configuration. Short-term testing did not permit evaluation of Coolside system availability.

Economic Performance (LIMB & Coolside)

Economic comparisons were made between LIMB, Coolside, and a wet scrubber with limestone injection and forced oxidation (LSFO). Assumptions on performance were SO_2 removal efficiencies of 60, 70, and 95% for LIMB, Coolside, and LSFO, respectively. EPRI TAG™ method was used. Exhibits 5-36 and 5-37 summarize the results.

Commercial Application

Both LIMB and Coolside technologies are applicable to most utility and industrial coal-fired units and provide alternatives to conventional wet flue gas desulfurization processes. LIMB and Coolside can be retrofitted with modest capital investment and downtime, and their space requirements are substantially less than for conventional flue gas sulfurization processes.

LIMB has been sold to an independent power plant in Canada. Babcock & Wilcox has signed 85 contracts (61 domestic, 24 foreign) for DLB-XCL® low-NO_x burners, representing 1,515 burners for 20,396-MWe of capacity.

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References

- T.R. Goots, M.J. DePero, and P.S. Nolan. *LIMB Demonstration Project Extension and Coolside Demonstration: Final Report.* Report No. DOE/PC/79798-T27. The Babcock & Wilcox Company. November 1992. (Available from NTIS as DE93005979.)
- D.C. McCoy et al. *The Edgewater Coolside Process Demonstration: A Topical Report.* Report No. DOE/PC/79798-T26. CONSOL, Inc. February 1992. (Available from NTIS as DE93001722.)
- *Coolside and LIMB: Sorbent Injection Demonstrations Nearing Completion.* Topical Report No. 2. U.S. Department of Energy and The Babcock & Wilcox Company. September 1990.
- *Public Design Report.* Report No. DOE/PC/79798-T2. The Babcock & Wilcox Company. December 1988. (LIMB/Coolside demonstration.) (Available from NTIS as DE92016131.)
- *Comprehensive Report to Congress on the Clean Coal Technology Program: LIMB Demonstration Project Extension.* The Babcock & Wilcox Company. Report No. DOE/FE-0085. U.S. Department of Energy. April 1987. (Available from NTIS as DE87009793.)

SO_x-NO_x-Rox Box™ Flue Gas Cleanup Demonstration Project

Project completed.

Participant
The Babcock & Wilcox Company

Additional Team Members
Ohio Edison Company—cofunder and host
Ohio Coal Development Office—cofunder
Electric Power Research Institute—cofunder
Norton Company—cofunder and SCR catalyst supplier
3M Company—cofunder and filter bag supplier
Owens Corning Fiberglas Corporation—cofunder and filter bag supplier

Location
Dilles Bottom, Belmont County, OH (Ohio Edison Company's R.E. Burger Plant, Unit No. 5)

Technology
The Babcock & Wilcox Company's SO_x-NO_x-Rox Box™ (SNRB™) process

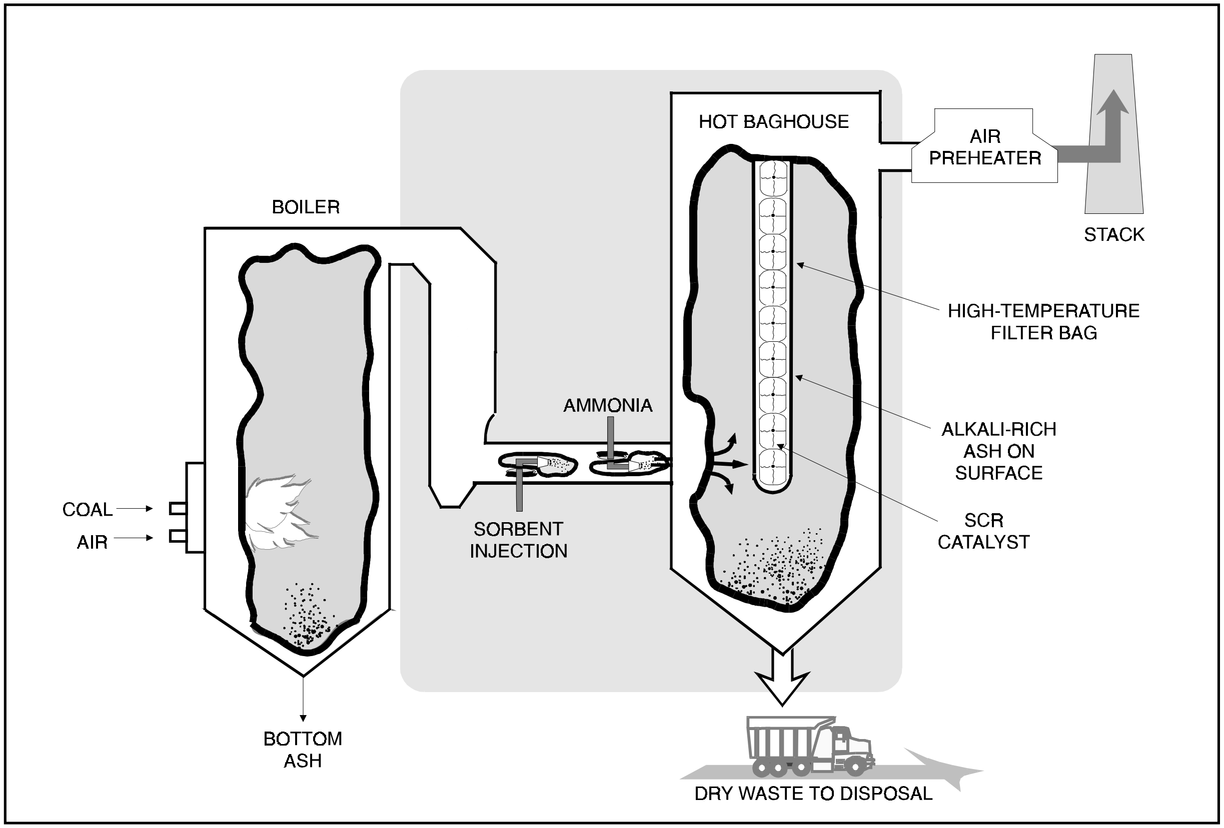
Plant Capacity/Production
5-MWe equivalent slipstream from a 156-MWe boiler

Coal
Bituminous coal blend, 3.7% sulfur average

Project Funding

Total project cost	$13,271,620	100%
DOE	6,078,402	46
Participant	7,193,218	54

Project Objective
To achieve greater 70% SO_2 removal and 90% or higher reduction in NO_x emissions while maintaining particulate emissions below 0.03 lb/10^6 Btu.

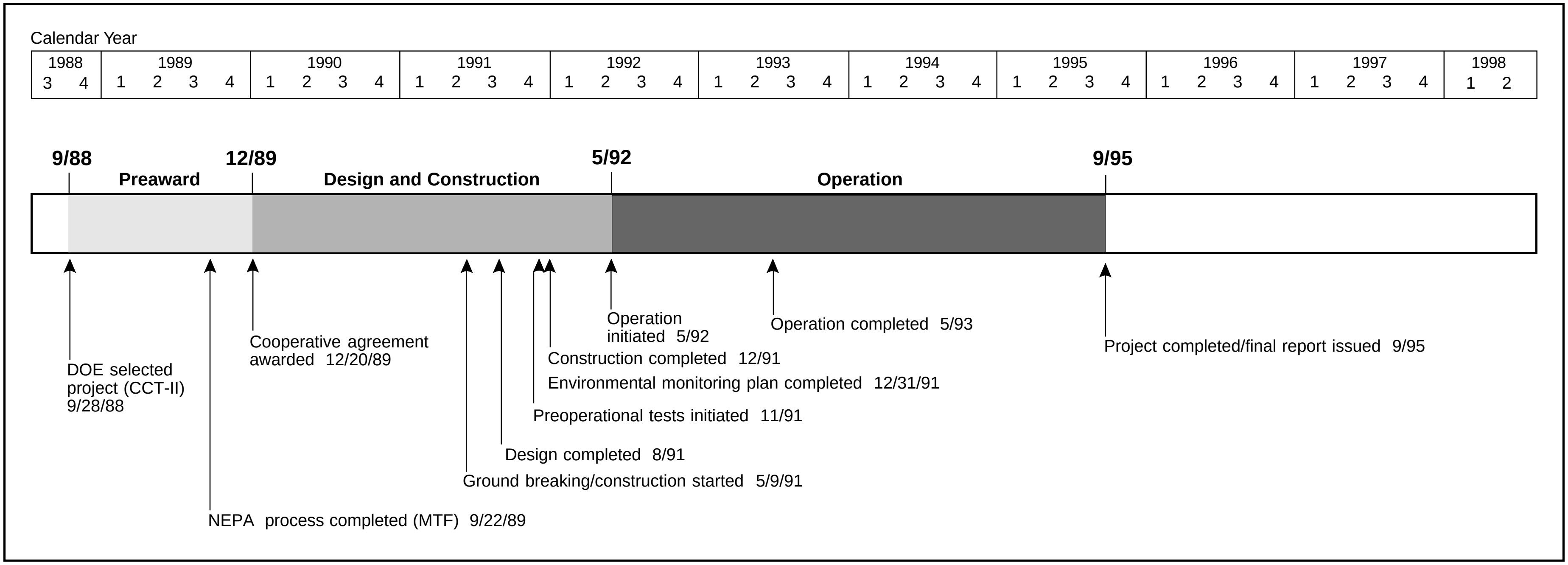


Technology/Project Description
The SNRB™ process combines the removal of SO_2, NO_x, and particulates in one unit—a high-temperature baghouse. SO_2 removal is accomplished using either calcium- or sodium-based sorbent injected into the flue gas. NO_x removal is accomplished by injecting ammonia (NH_3) to selectively reduce NO_x in the presence of a selective catalytic reduction (SCR), catalyst. Particulate removal is accomplished by high-temperature fiber bag filters.

The 5-MWe SNRB™ demonstration unit is large enough to demonstrate commercial-scale components while minimizing the demonstration cost. Operation at this scale also permitted cost-effective control of the flue gas temperature, which allowed for evaluation of performance over a wide range of sorbent injection and baghouse operating temperatures. Thus several different arrangements for potential commercial installations could be simulated.

The SNRB™ process was operated for approximately 2,300 hours. Through this effort, SNRB™ demonstrated the technical and economic feasibility of achieving more than 80% SO_2 removal, more than 90% NO_x removal, and 99% particulate removal at lower capital, operating, and maintenance costs than those for a combination of conventional systems. The demonstration was conducted at Ohio Edison Company's R.E. Burger Plant, Unit No. 5, in Dilles Bottom, OH.

SO_x-NO_x-Rox Box and SNRB are trademarks of The Babcock & Wilcox Company.



Results Summary

Environmental

- SO_2 removal efficiency of 80% was achieved with commercial-grade lime at a calcium-to-sulfur (Ca/S) molar ratio of 2.0 and temperature of 800–850 ºF.
- SO_2 removal efficiency of 90% was achieved with sugar hydrated and lignosulfonate hydrated lime at a Ca/S molar ratio of 2.0 and temperature of 800–850 ºF.
- SO_2 removal efficiency of 80% was achieved with sodium bicarbonate at a sodium-to-sulfur (Na_2/S) molar ratio of 1.0 and temperature of 425 ºF.
- SO_2 emissions were reduced to less than 1.2 lb/10^6 Btu with 3–4% sulfur coal with a Ca/S molar ratio as low as 1.5 and NA_2/S molar ratio of 1.0.
- Injection of calcium-based sorbents directly upstream of the baghouse at 825–900 ºF resulted in higher overall SO_2 removal than injection further upstream at temperatures up to 1,200 ºF.
- NO_x reduction of 90% was achieved with an NH_3/NO_x molar ratio of 0.9 and temperature of 800–850 ºF.
- Air toxic removal efficiency was comparable to that of an electrostatic precipitator (ESP), except that hydrogen fluoride (HF) was reduced by 84% and hydrogen chloride (HCl) by 95%.

Operational

- Calcium utilization was 40–45% for SO_2 removals of 85–90%.
- Norton Company’s NC-300 zeolite SCR catalyst showed no appreciable physical degradation or change in catalyst activity over the course of the demonstration.
- No excessive wear or failures occurred with the filter bags tested: 3M’s Nextel ceramic fiber filter bag and Owens Corning Fiberglas’s S-Glass filter bag.

Economic

- Capital cost in 1994 constant dollars for a 250-MWe retrofit was \$233/kW, assuming 3.5% sulfur coal and baseline NO_x generation of 1.2 lb/10^6 Btu.

Project Summary

SNRB™ incorporates two successful technology development efforts that offer distinct advantages over other control technologies. High-temperature filter bags and circular monolith catalyst developments enabled multiple emission control in a single component with a low plant-area space requirement. As a postcombustion control system, it is simple to operate. The high-temperature bag provides a clean, high-temperature environment compatible with effective SCR operation and a surface for enhanced SO_2/sorbent contact (creates a sorbent cake on the surface). Particulate control, which is receiving increasing attention, is typical of the superior performance offered by pulsed jet baghouses.

Environmental Performance

Four different sorbents were tested for SO_2 capture. Calcium-based sorbents included commercial grade hydrated lime, sugar-hydrated lime, and lignosulfonate-hydrated lime. In addition, sodium bicarbonate was tested. The optimal location for injecting the sorbent into the flue gas was immediately upstream of the baghouse. Effectively, the SO_2 was captured by the sorbent in the form of a filter cake on the filter bags (along with fly ash).

With the baghouse operating above 830 ºF, injection of commercial-grade hydrated lime at Ca/S molar ratio of 1.8 and above resulted in SO_2 removals of over 80%. At a Ca/S of molar ratio of 2.0, performance of the sugar-hydrated lime and lignosulfonate-hydrated lime increased performance by approximately 8%, for overall removal of approximately 90%. SO_2 removal of 85–90% was obtained with calcium utilization of 40–45%. Injection of the calcium-based sorbents directly upstream of the baghouse at 825–900 ºF resulted in higher overall SO_2 removal than injection further upstream at temperatures up to 1,200 ºF.

SO_2 removal using sodium bicarbonate was 80% at an Na_2/S molar ratio of 1.0 and 98% at an Na_2/S molar ratio of 2.0 at a significantly reduced baghouse temperature of 450–460 ºF. SO_2 emissions while burning a 3–4% sulfur coal were reduced to less than 1.2 lb/10^6 Btu with a Ca/S molar ratio as low as 1.5 and Na_2/S molar ratio less than 1.0.

To capture NO_x, ammonia was injected between the sorbent injection point and the baghouse. The ammonia and NO_x reacted to form nitrogen and water in the presence of Norton Company's NC-300 series zeolite SCR catalyst. With the catalyst being located inside the filter bags, it was well protected from potential particulate erosion or fouling. The sorbent reaction products, unreacted lime, and fly ash were collected on the filter bags and thus removed from the flue gas.

NO_x emissions reduction of 90% was readily achieved with ammonia slip limited to less than 5 ppm. This performance reduced NO_x emissions to less than 0.10 lb/10^6 Btu. NO_x reduction was insensitive to temperatures over the catalyst design temperature range of 700–900 ºF. Catalyst space velocity (volumetric gas flow/catalyst volume) had a minimal effect on NO_x removal over the range evaluated.

Turndown capability for tailoring the degree of NO_x reduction by varying the rate of ammonia injection was demonstrated for a range of 50–95% NO_x reduction. No appreciable physical degradation or change in the catalyst activity was observed over the duration of the test program. The degree of oxidation of SO_2 to SO_3 over the zeolite catalyst appeared to be less than 0.5%. (SO_2 oxidation is a concern for SCR catalysts containing vanadium.) Leach potential analysis of the catalyst after completion of the field test showed that the catalyst remained nonhazardous for disposal.

▲ The demonstration baghouse is installed on the back side of the power plant. Workers stand by the catalyst holder tube prior to lifting it into the penthouse.

Particulate emissions were consistently below NSPS standards of 0.03 lb/10^6 Btu, with an average over 30 baghouse particulate emission measurements of 0.018 lb/10^6 Btu, which corresponds to a collective efficiency of 99.89%. Hydrated lime injection increased the baghouse inlet particulate loading from 5.6 to 16.5 lb/10^6 Btu. Emissions testing with and without the SCR catalyst installed revealed no apparent differences in collection efficiency. On-line cleaning with a pulse air pressure of 30–40 lb/in^2 was sufficient for cleaning the bag/catalyst assemblies. Typically, one of five baghouse modules in service was cleaned every 30–150 minutes.

A comprehensive air toxics emissions monitoring test was performed at the end of the SNRB™ demonstration test program. The targeted emissions monitored included trace metals, volatile organic compounds, semi-volatile organic compounds, aldehydes, halides, and radionuclides. These species were a subset of the 189 substances identified in the CAAA. Measurements of mercury speciation, dioxins, and furans were unique features of this test program. The emissions control efficiencies achieved for various air toxics by the SNRB™ system were generally comparable to those of the conventional ESP at the power plant. However, the SNRB™ system did reduce HCl by an average of 95% and HF emissions by an average of 84%, whereas the ESP had no effect on these constituents.

Operation of the SNRB™ demonstration resulted in the production of approximately 830 tons of fly ash and by-product solids. An evaluation of potential uses for the by-product showed that the material might be used for agricultural liming (if pelletized). Also, the solids potentially could be used as a partial cement replacement to lower the cost of concrete.

Operational Performance

A 3,800-hour durability test of three fabric filters was completed at the Filter Fabric Development Test Facility in Colorado Springs in December 1992. No signs of failure were observed. All of the demonstration tests were conducted using the 3M Company Nextel ceramic fiber filter bags or the Owens Corning Fiberglas S-Glass filter bags. No excessive wear or failures occurred in over 2,000 hours of elevated temperature operation.

Economic Performance

For a 250-MWe boiler fired with 3.5% sulfur coal and NO_x emissions of 1.2 lb/10^6 Btu, the projected capital cost of an SNRB™ system is approximately $233/kW (1994 constant dollars), including various technology and project contingency factors. A combination of fabric filter, SCR, and wet scrubber for achieving comparable emissions control has been estimated at $360–400/kW. Variable operating costs are dominated by the cost of the SO_2 sorbent for a system designed for 85–90% SO_2 removal. Fixed operating costs primarily consist of system operating labor and projected labor and material for the hot baghouse and ash-handling systems.

Commercial Applications

Commercialization of the technology is expected to develop with an initial larger scale application equivalent to 50–100-MWe. The focus of marketing efforts is being tailored to match the specific needs of potential industrial, utility, and independent power producers for both retrofit and new plant construction. SNRB™ is a flexible technology that can be tailored to maximize control of SO_2, NO_x, or combined emissions to meet current performance requirements while providing flexibility to address future needs.

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References

- *SO_x-NO_x-Rox Box™ Flue Gas Cleanup Demonstration Final Report*. Report No. DOE/PC/89656-T1. The Babcock & Wilcox Company. September 1995. (Available from NTIS as DE96003839.)
- *5 MWe SNRB™ Demonstration Facility: Detailed Design Report.* The Babcock & Wilcox Company. November 1992.
- *Comprehensive Report to Congress on the Clean Coal Technology Program: SO_x-NO_x-Rox Box™ Flue Gas Cleanup Demonstration Project.* The Babcock & Wilcox Company. Report No. DOE/FE-0145. U.S. Department of Energy. November 1989. (Available from NTIS as DE90004458.)

▲ Workers lower one of the catalyst holder tubes into a mounting plate in the penthouse of the high-temperature baghouse.

Enhancing the Use of Coals by Gas Reburning and Sorbent Injection

Project completed.

Participant

Energy and Environmental Research Corporation

Additional Team Members

Gas Research Institute—cofunder

State of Illinois, Department of Commerce & Community Affairs—cofunder

Illinois Power Company—host

City Water, Light and Power—host

Locations

Hennepin, Putnam County, IL (Illinois Power Company's Hennepin Plant, Unit No. 1)

Springfield, Sangamon County, IL (City Water, Light and Power's Lakeside Station, Unit No. 7)

Technology

Energy and Environmental Research Corporation's gas reburning and sorbent injection (GR–SI) process

Plant Capacity/Production

Hennepin: tangential-fired 80-MWe (gross), 71-MWe (net)

Lakeside: cyclone-fired 40-MWe (gross), 33-MWe (net)

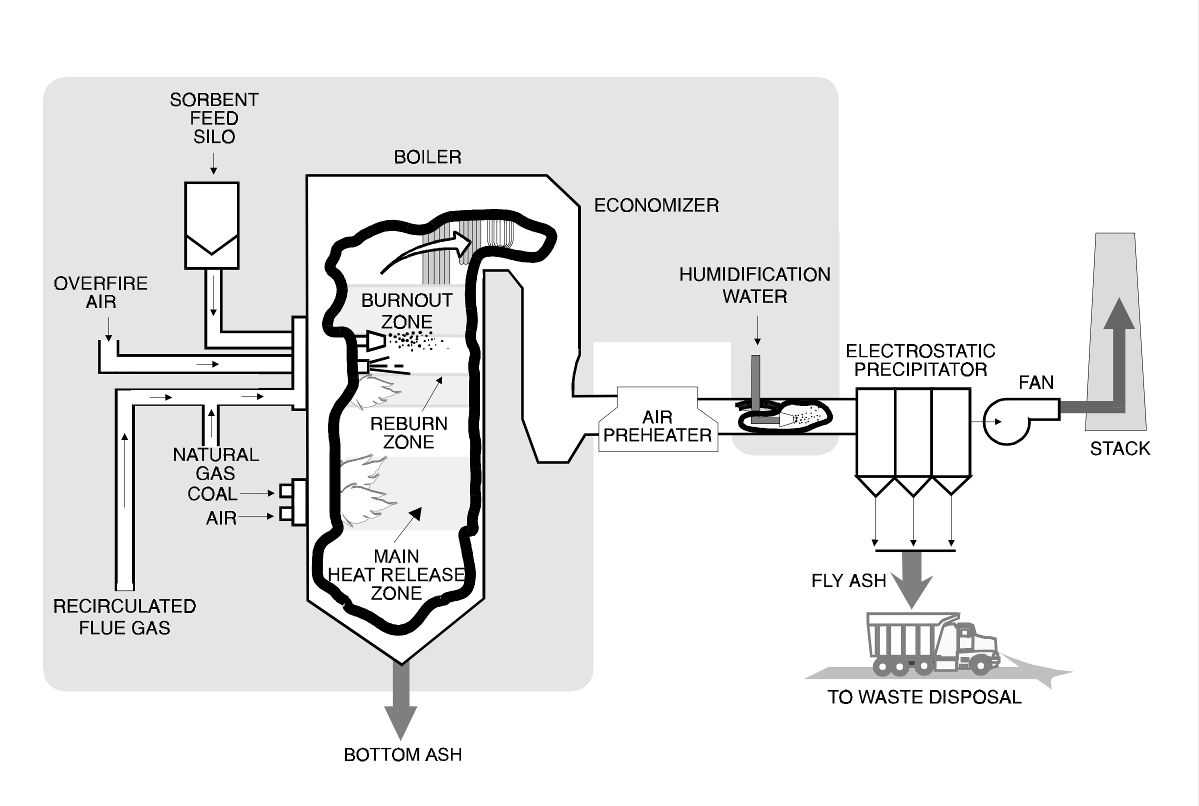
Coal

Illinois bituminous, 3.0% sulfur

Project Funding

Total project cost	$37,588,955	100%
DOE	18,747,816	50
Participant	18,841,139	50

PromiSORB is a trademark of Energy and Environmental Research



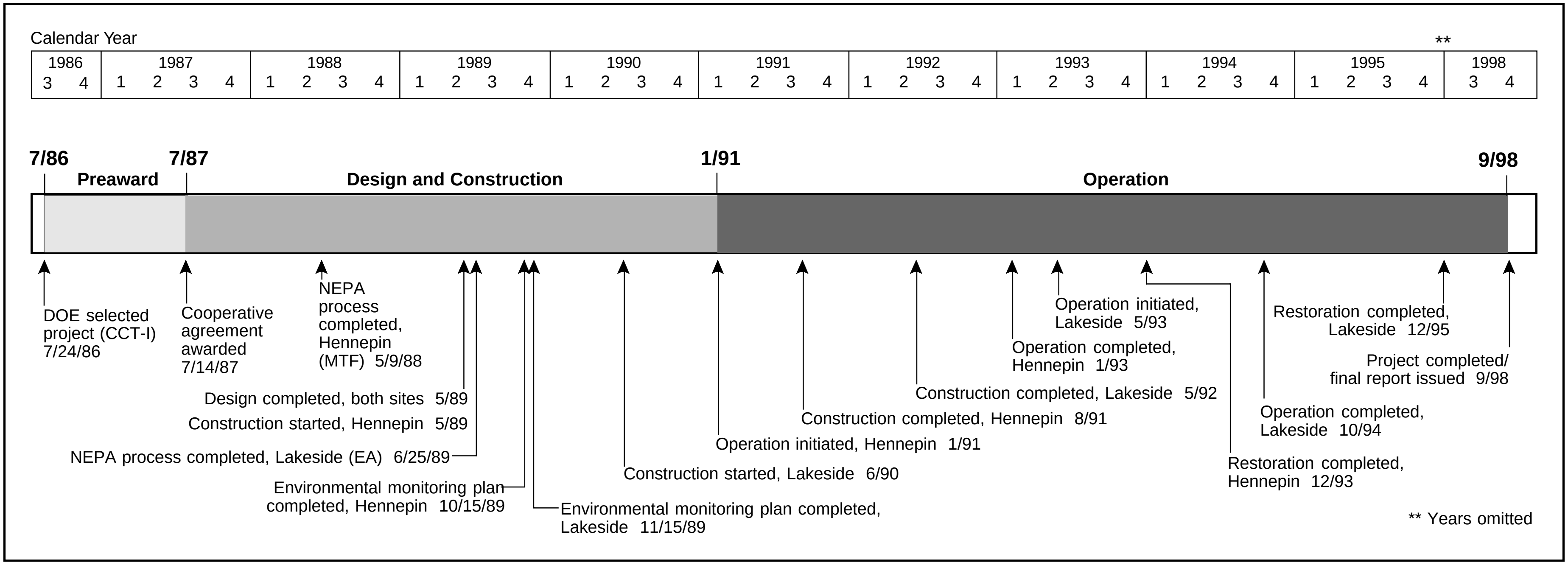
Project Objective

To demonstrate gas reburning to attain at least 60% NO_x reduction along with sorbent injection to capture at least 50% of the SO_2 on two different boiler configurations—tangentially fired and cyclone-fired—while burning high-sulfur midwestern coal.

Technology/Project Description

In this process, 80–85% of the fuel was coal and was supplied to the main combustion zone. The remaining 15–20% of the fuel, provided by natural gas, bypassed the main combustion zone and was injected above the main burners to form a reducing (reburning) zone in which NO_x was converted to nitrogen. A calcium compound (sorbent) was injected in the form of dry, fine particulates above the reburning zone in the boiler. Lime ($Ca(OH)_2$) was the sorbent tested at both sites. This project demonstrated the GR–SI process on two separate boilers representing two different firing configurations—a tangentially-fired, 80-MWe (gross) boiler at Illinois Power Company's Hennepin Plant in Hennepin, IL, and a cyclone-fired, 40-MWe (gross) boiler at City Water, Light and Power's Lakeside Station in Springfield, IL. Illinois bituminous coal containing 3% sulfur was the test coal for both Hennepin and Lakeside.

A comprehensive test program was conducted at each of the two sites, operating the equipment over a wide range of boiler conditions. Over 1,500 hours of operation was achieved, enabling a substantial amount of data to be obtained. Intensive measurements were taken



to quantify the reductions in NO_x and SO_2 emissions, the impact on boiler equipment and operability, and all factors influencing costs.

Results Summary

Environmental

- On the tangentially fired boiler, GR–SI NO_x reductions of up to 75% were achieved, and an average 67% reduction was realized at an average gas heat input of 18%.
- GR–SI SO_2 removal efficiency on the tangentially fired boiler averaged 53% with hydrated lime at a calcium-to-sulfur (Ca/S) molar ratio of 1.75 (corresponding to a sorbent utilization of 24%).
- On the cyclone-fired boiler, GR–SI NO_x reductions of up to 74% were achieved, and an average 66% reduction was realized at an average gas heat input of 22%.
- GR–SI SO_2 removal efficiency on the cyclone-fired boiler averaged 58% with hydrated lime at a Ca/S molar ratio of 1.8 (corresponding to a sorbent utilization of 24%).
- Particulate emissions were not a problem on either unit undergoing demonstration, but humidification had to be introduced at Hennepin to enhance ESP performance.
- Three advanced sorbents tested achieved higher SO_2 capture efficiencies than the baseline Linwood hydrated lime. PromiSORB™ A achieved 53% SO_2 capture efficiency and 31% utilization without GR at a Ca/S molar ratio of 1.75. Under the same conditions, PromiSORB™ B achieved 66% SO_2 reduction and 38% utilization, and High-Surface-Area Hydrated Lime achieved 60% SO_2 reduction and 34% utilization.

Operational

- Boiler efficiency decreased by approximately 1% as a result of increased moisture formed in combustion from natural gas use.
- There was no change in boiler tube wastage, tube metallurgy, or projected boiler life.

Economic

- Capital cost for gas reburning (GR) was approximately \$15/kW plus the gas pipeline cost, if not in place.
- Operating costs for GR were related to the gas/coal cost differential and the value of SO_2 emission allowances (because GR replaces some coal with gas, it also reduces SO_2 emissions).
- Capital cost for sorbent injection (SI) was approximately \$50/kW.
- Operating costs for SI were dominated by the cost of sorbent and sorbent/ash disposal costs. SI was estimated to be competitive at \$300/ton of SO_2 removed.

Project Summary

The GR–SI project demonstrated the success of gas reburning and sorbent injection technologies in reducing NO_x and SO_2 emissions. The process design conducted early in the project combined with the vast amount of data collected during the testing created a database capable of applying the technology to all major coal-firing configurations (tangential-, cyclone-, and wall-fired) on both utility and industrial units. The emissions control and performance can be accurately projected as can the capital and operating costs.

Environmental Performance (Hennepin)

Operational testing, which included optimization testing and long-term testing, was conducted between January 1991 and January 1993. The GR–SI long-term demonstration tests were carried out from January 1992 to October 1992 to verify the system performance over an extended period. The unit was operated at constant loads and with the system under dispatch operation where load was varied to meet plant power output requirements. With the system under dispatch, the load fluctuated over a wide range from 40-MWe to a maximum load of 75-MWe. Over the long-term demonstration period, the average gross power output was 62-MWe.

For long-term demonstration testing, the average NO_x reduction was approximately 67%. The average SO_2 removal efficiency was over 53% at a Ca/S molar ratio of 1.75. (Linwood hydrated lime was used throughout these tests except for a few days when Marblehead lime was used.) CO emissions were below 50 ppm in most cases but were higher during operation at low load.

A significant reduction in CO_2 was also measured. This was due to partial replacement of coal with natural gas having a lower carbon-to-hydrogen ratio. This cofiring with 18% natural gas resulted in a theoretical CO_2 emissions reduction of nearly 8% from the coal-fired baseline level. With flue gas humidification, electrostatic precipitator (ESP) collection efficiencies greater than 99.8% and particulate emissions less than 0.025 lb/10^6 Btu were measured even with an increase in inlet particulate loading resulting from sorbent injection. These levels were comparable to measured baseline emissions of 0.035 lb/10^6 Btu and a collection efficiency greater than 99.5%.

Following the completion of the long-term tests, three specially prepared sorbents were tested. Two were manufactured by the participant and contained proprietary additives to increase their reactivity toward SO_2 and were referred to as PromiSORB™ A and B. The Illinois State Geological Survey developed the other sorbent—High-Surface-Area Hydrated Lime in which alcohol is used to form a material that gives rise to a much higher surface area than that of conventionally hydrated limes.

The SO_2 capture without GR, at a nominal 1.75 Ca/S molar ratio, was 53% for PromiSORB™ A, 66% for PromiSORB™ B, 60% for High-Surface-Area Hydrated Lime, and 42% for Linwood lime. At a 2.6 Ca/S molar ratio, the PromiSORB™ B yielded 81% SO_2 removal efficiency.

Environmental Performance (Lakeside)

Parametric tests were conducted in three series: GR parametric tests, SI parametric tests, and GR–SI optimization tests. A total of 100 GR parametric tests were conducted at boiler loads of 33-, 25-, and 20-MWe. Gas heat input varied from 5-26%. The GR parametric tests achieved a NO_x reduction of approximately 60% at a gas heat input of 22–23%. Additional flow modeling and computer modeling studies indicated that smaller reburning fuel jet nozzles could increase reburning fuel mixing and thus improve the NO_x reduction performance.

A total of 25 SI parametric tests were conducted to isolate the effects of sorbent on boiler performance and operability. Results showed that SO_2 reduction level varied with load because of the effect of temperature on the sulfation reaction. At a Ca/S molar ratio of 2.0, 44% SO_2 reduction was achieved at full load (33-MWe); 38% SO_2 reduction was achieved at mid-load (25-MWe); and 32% SO_2 reduction was achieved at low load (20-MWe).

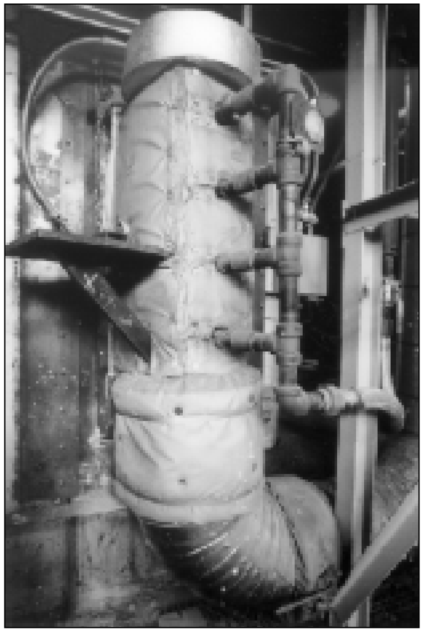
In the GR–SI optimization tests, the two technologies were integrated. Modifications were made to the reburning fuel injection nozzles based on the results of the initial GR parametric tests and flow modeling studies. The total cross-sectional area of the reburning jets was

▲ The flexible lime-sorbent distribution lines lead from the sorbent splitter to the top of the cyclone-fired boiler at Lakeside Station.

decreased by 32% to increase the reburning jet's penetration characteristics. The decrease in nozzle diameter increased NO_x reduction by an additional 3–5% compared to the initial parametric tests. With GR–SI, total SO_2 reductions resulted from partial replacement of coal with natural gas and sorbent injection. At a gas heat input of 22% and Ca/S molar ratio of 1.8, average NO_x reduction during the long-term testing of GR–SI was 66% and the average SO_2 reduction was 58%.

Operational Performance (Hennepin/Lakeside)

Sorbent injection increased the frequency of sootblower operation but did not adversely affect boiler efficiency or equipment performance. Gas reburning decreased boiler efficiency by approximately 1.0% because of the increase in moisture formed with combustion of natural gas. Examination of the boiler before and after testing showed no measurable change in tube wear or metallurgy. Essentially, the scheduled life of the boiler was not compromised.



▲ The natural gas injector was installed on the corner of Hennepin Station's tangentially fired boiler.

The ESPs adequately accommodated the changes in ash loading and resistivity with the presence of sorbent in the ash. No adverse conditions were found to exist. But as mentioned, humidification had to be added at Hennepin to achieve acceptable ESP performance with GR–SI.

Economic Performance (Hennepin/Lakeside)

Capital and operating costs depend largely on site-specific factors, such as gas availability at the site, coal/gas cost differential, SO_2 removal requirements, and value of SO_2 allowances. It was estimated that for most installation, a 15% gas heat input will achieve 60% NO_x reduction. The capital cost for such a GR installation was estimated at $15/kW for 100-MWe and larger plants plus the cost of the gas pipeline (if required). Operating costs were almost entirely related to the differential cost of the gas over the coal as reduced by the value of SO_2 emission allowances.

The capital cost estimate for SI was $50/kW. Operating costs for SI were dominated by the cost of the sorbent and sorbent/ash disposal costs. SI was projected to be cost competitive at $300/ton of SO_2 removed.

Commercial Applications

The GR–SI process is a unique combination of two separate technologies. The commercial applications for these technologies, both separately and combined, extend to both utility companies and industry in the United States and abroad. In the United States alone, these two technologies can be applied to more than 900 pre-NSPS utility boilers; the technologies also can be applied to new utility boilers. With NO_x and SO_2 removal exceeding 60% and 50%, respectively, these technologies have the potential to extend the life of a boiler or power plant and also provide a way to use higher sulfur coals.

Illinois Power has retained the gas-reburning system and City Water, Light & Power has retained the full technology for commercial use.

The project was one of two receiving the Air and Waste Management Association's 1997 J. Deanne Sensenbaugh Award.

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References

- *Enhancing the Use of Coals by Gas Reburning and Sorbent Injection; Volume 1–Program Overview. February 1997.*
- *Enhancing the Use of Coals by Gas Reburning–Sorbent Injection: Volume 4: Gas Reburning Sorbent Injection at Lakeside Unit 7, City Water, Light and Power, Springfield, Illinois.* Final Report. Energy and Environmental Research Corporation. March 1996. Report No. DOE/PC/79796-T48-Vol.4. (Available from NTIS as DE96011869.
- *Enhancing the Use of Coals by Gas Reburning–Sorbent Injection; Long Term Testing Period, September 1, 1991–January 15, 1993.* Report No. DOE/PC/79796-T40. Energy and Environmental Research Corporation. February 1995. (Available from NTIS as DE95011481.)
- *Enhancing the Use of Coals by Gas Reburning and Sorbent Injection; Volume 2: Gas Reburning–Sorbent Injection at Hennepin Unit 1, Illinois Power Company.* Report No. DOE/PC/79796-T38-Vol. 2. Energy and Environmental Research Corporation. October 1994. (Available from NTIS as DE95009448.)
- *Enhancing the Use of Coals by Gas Reburning and Sorbent Injection; Volume 3: Gas Reburning–Sorbent Injection at Edwards Unit 1, Central Illinois Light Company.* Report No. DOE/PC/79796-T38-Vol. 3. Energy and Environmental Research Corporation. October 1994. (Available from NTIS as DE95009447.)
- *Clean Coal Technology: Reduction of NO_x and SO_2 Using Gas Reburning, Sorbent Injection, and Integrated Technologies.* Topical Report No. 3, Revision 1. U.S. Department of Energy and Energy and Environmental Research Corporation. September 1993. (Available from NTIS as DE94007444.)
- *Comprehensive Report to Congress on the Clean Coal Technology Program: Enhancing the Use of Coals by Gas Reburning and Sorbent Injection.* Energy and Environmental Research Corporation. Report No. DOE/FE-0087. U.S. Department of Energy. May 1987. (Available from NTIS as DE87010815.)

Integrated Dry NO_x/SO_2 Emissions Control System

Project completed.

Participant

Public Service Company of Colorado

Additional Team Members

Electric Power Research Institute—cofunder
Stone and Webster Engineering Corp.—engineer
The Babcock & Wilcox Company—burner developer
Fossil Energy Research Corporation—operational tester
Western Research Institute—flyash evaluator
Colorado School of Mines—bench-scale engineering researcher and tester
NOELL, Inc.—urea-injection system provider

Location

Denver, Denver County, CO (Public Service Company of Colorado's Arapahoe Station, Unit No. 4)

Technology

The Babcock & Wilcox Company's DRB-XCL® low-NO_x burners, in-duct sorbent injection, and furnace (urea) injection

Plant Capacity/Production

100-MWe

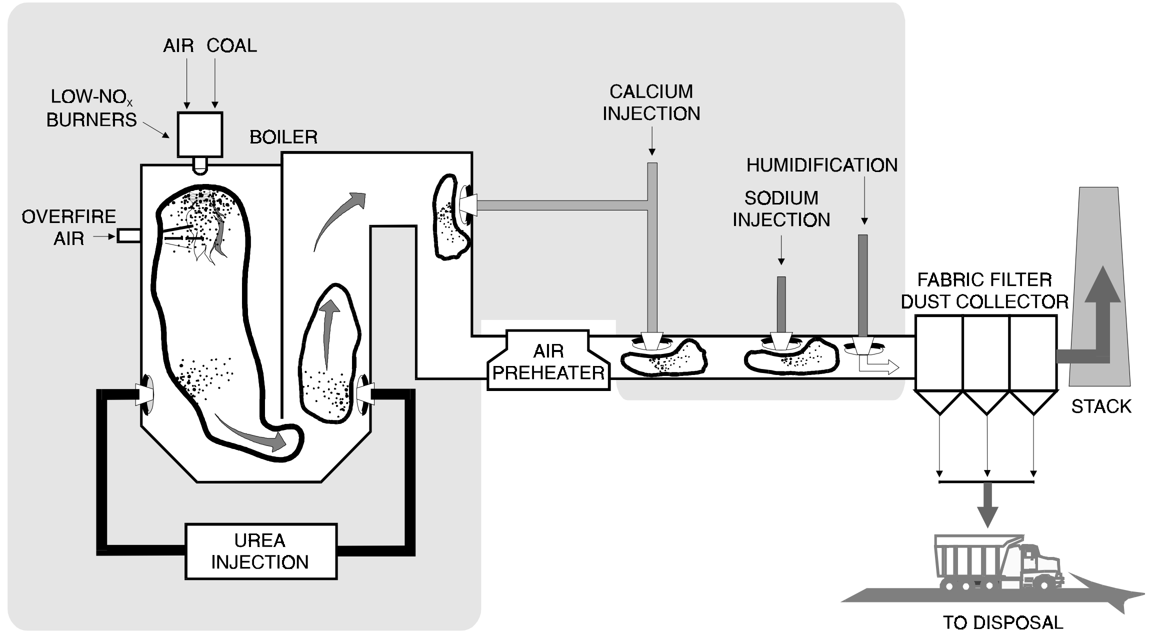
Coal

Colorado bituminous, 0.4% sulfur
Wyoming subbituminous (short test), 0.35% sulfur

Project Funding

Total project cost	$27,411,462	100%
DOE	13,705,731	50
Participant	13,705,731	50

DRB-XCL is a registered trademark of The Babcock & Wilcox Company.



Project Objective

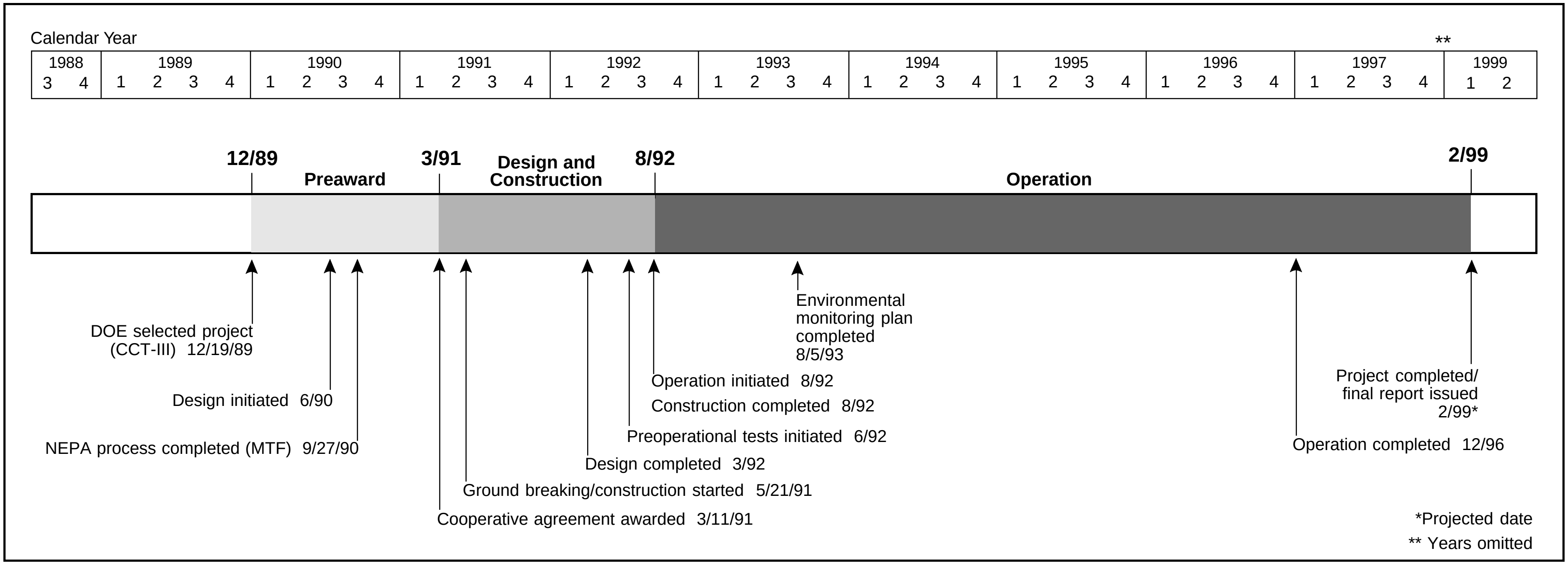
To demonstrate the integration of five technologies to achieve up to 70% reduction in NO_x and SO_2 emissions; more specifically, to assess the integration of a down-fired low-NO_x burner with in-furnace urea injection for additional NO_x removal and dry sorbent in-duct injection with humidification for SO_2 removal.

Technology/Project Description

All of the testing used Babcock & Wilcox's low-NO_x DRB-XCL® down-fired burners with overfire air. These burners control NO_x by injecting the coal and the combustion air in an oxygen-deficient environment. Additional air was introduced via overfire air ports to complete the combustion process and further enhance NO_x removal. A urea-based selective noncatalytic reduction (SNCR) system was tested to determine how much additional NO_x can be removed from the combustion gas.

Two types of dry sorbents were injected into the ductwork downstream of the boiler to reduce SO_2 emissions. Either calcium was injected upstream of the boiler economizer or sodium downstream of the air heater. Humidification downstream of the dry sorbent injection was incorporated to aid SO_2 capture and lower flue gas temperature and gas flow before entering the fabric filter dust collector.

The systems were installed on Public Service Company of Colorado's Arapahoe Station Unit No. 4, a 100-MWe down-fired, pulverized-coal boiler with roof-mounted burners.



Results Summary

Environmental

- With maximum overfire air (24% of total combustion air), a NO_x reduction of 62–69% was achieved across the 50–110-MWe load range.
- DRB-XCL® burners with minimum overfire air reduced NO_x emissions by more than 63% under steady state conditions.
- NO_x reductions were decreased by 10–25% under load-following conditions.
- The SNCR system, using both stationary and retractable injection lances in the furnace, provided NO_x removal of 30–50% at an ammonia (NH_3) slip of 10 ppm, thus increasing performance of the total NO_x control system to greater than 80% NO_x reduction.
- SO_2 removal with calcium-based dry sodium injection into the boiler at approximately 1,000 ºF was less than 10%, and with injection into the fabric filter duct, SO_2 removal was less than 40% at a Ca/S molar ratio of 2.0.
- Sodium bicarbonate injection before the air heater demonstrated a long-term SO_2 removal of approximately 70% at a normalized stoichiometric ratio (NSR) of 1.0.
- Sodium sesquicarbonate injection ahead of the fabric filter achieved 70% SO_2 removal at an NSR of 2.0.
- NO_2 emissions were generally higher when using sodium biocarbonate than when using sodium sesquicarbonate.
- Integrated SNCR and sodium dry sorbent injection tests showed reduced NH_3 and NO_2 emissions.
- During four series of air toxics tests, the fabric filter successfully removed nearly all trace metal emissions and 80% of the mercury.

Operational

- Arapahoe Unit No. 4 operated more than 34,000 hours after combustion modifications were complete.
- Availability factor was over 91%.
- Operational test objectives were met or exceeded.
- Control system modifications and additional operator training may be necessary to improve NO_x control under load-following conditions.
- Buildup of a hard ash cake on the fabric filter occurred during operation of dry sorbent injection of calcium hydroxide with humidification.
- Temperature differential between the top and bottom surfaces of the Advanced Retractable Injection Lances (ARIL) caused the lances to bend downwards 12–18 inches. Alternative designs corrected the problem.
- Concurrent operation of SNCR and the dry sodium injection system caused an NH_3 odor problem around the ash silo, which appeared to be related to the rapid change in pH due to the sodium in the ash.

Economic

- Data not available.

Project Summary

The Integrated Dry NO_x/SO_x Emissions Control System combines five major control technologies to form an integrated system to control both NO_x and SO_2. The low-NO_x combustion system consists of 12 Babcock & Wilcox DRB-XCL® low-NO_x burners installed on the boiler roof. The low-NO_x combustion system also incorporated three Babcock & Wilcox dual-zone NO_x ports added to each side of the furnace approximately 20 feet below the boiler roof. These ports injected up to 25% of the total combustion air through the furnace sidewalls.

Additional NO_x control was achieved with the urea-based SNCR system. The SNCR when used with the low-NO_x combustion system would allow the goal of 70% NO_x reduction to be reached. Further, the SNCR system was an important part of the integrated system, interacting synergistically with the dry sorbent injection (DSI) system to reduce NO_2 formation and ammonia slip.

Initially the SNCR was designed and installed to incorporate two levels of injectors with 10 injectors at each level, with the exact location being based on temperature profiles that existed with the original combustion system. However, the retrofit low-NO_x combustion system resulted in a decrease in furnace exit gas temperature by approximately 200 ºF, thus moving one injector level out of the temperature regime needed for effective SNCR operation. With only one operational injector level, load-following performance was compromised.

In order to achieve the desirable NO_x reduction at low loads, two alternatives were explored. The first approach was to substitute ammonia for urea. It was shown that ammonia was more effective than urea at low-loads. An on-line urea-to-ammonia conversion system was installed and resulted in improved low-load performance, but the improvement was not as large as desired for the lowest load (60-MWe). The second approach was to install injectors in the higher temperature regions of the furnace. This was achieved by installing two NOELL ARIL lances into the furnace through two unused

▲ Public Service Company of Colorado demonstrated low-NO_x burners, in-duct sorbent injection, and SNCR at Arapahoe Station near Denver.

sootblower ports. Each lance was nominally 4 inches in diameter and approximately 20 feet in length with a single row of nine injection nozzles. Each injection nozzle consisted of a fixed air orifice and a replaceable liquid orifice. The ability to change orifices allowed not only for removal and cleaning but adjustment of the injection pattern along the length of the lance in order to compensate for any significant mal distributions of flue gas velocity, temperature, or baseline NO_x concentration. One of the key features of the ARIL system was its ability to rotate, thus providing a high degree of flexibility in optimizing SNCR performance.

The SO_2 control system was a direct sorbent injection system that could inject either calcium- or sodium-based reagents into the flue gas upstream of the fabric filter. Sorbent was injected into three locations: (1) air heater exit where the temperature was approximately 260 ºF, (2) air heater entrance where the temperature was approximately 600 ºF, or (3) the boiler economizer region where the flue gas temperature was approximately 1,000 ºF. To improve SO_2 removal with calcium hydroxide, a humidification system capable of achieving 20 ºF approach-to-saturation was installed approximately 100 feet ahead of the fabric filter. The system designed by Babcock & Wilcox included 84 I-Jet nozzles that can inject up to 80 gal/min into the flue gas duct work.

Environmental Performance

The combined DRB-XCL® burner and minimum overfire air reduced NO_x emissions by over 63% under steady-state conditions and with carefully supervised operations. Under load-following conditions, NO_x emissions were about 10–25% higher. At maximum overfire air (4% of total combustion air), the low-NO_x combustion system reduced NO_x emissions by 62–69% across the load range (60–110-MWe). The results indicated that the low-NO_x burners were responsible for most of the NO_x reduction.

The original design of two rows of injector nozzles proved relatively ineffective because one row of injectors was in a region where the flue gas temperature was too low for effective operation. At full load, the original design achieved NO_x reduction of 45%. However, the performance decreased significantly as load decreased; at 60-MWe, NO_x removal was limited to about 11% with an ammonia slip of 10 ppm. The addition of the retractable lances improved low-load performance of the urea-based SNCR injection system. The ability to follow the temperature window by rotating the ARIL lances proved to be an important feature in optimizing performance. As a result, the SNCR system obtained NO_x removal of 30–50%, at a NH_3 slip limited to 10 ppm at the fabric filter inlet, thus increasing the total NO_x control system reduction to greater than 80%, significantly exceeding the goal of 70%.

Testing of calcium hydroxide injection at the economizer without humidification resulted in SO_2 removal in the range of 5–8% at a Ca/S molar ratio of 2.0. Higher SO_2 removal was achieved with duct injection of calcium hydroxide and humidification, with SO_2 removals approaching 40% at a Ca/S molar ratio of 2.0 and approach-to-saturation temperature of 20–30 ºF. Sodium-based reagents were found to be much more effective than calcium-based sorbents and achieved significantly higher SO_2 removals during dry injection. Sodium bicarbonate injection before the air heater demonstrated short-time SO_2 removals of 80%. Long-term reductions of 70% were achieved with an NSR of 1.0. Sodium sesquicarbonate achieved 70% removal at an NSR of 2.0 when injected ahead of the fabric filter. A disadvantage of the sodium-based process was that it converted some existing NO to NO_2. Even though 5–10% of the NO_x was reduced during the conversion process, the net NO_2 exiting at the stack was increased. While NO is colorless, small quantities of brown/orange NO_2 caused a visible plume.

A major objective was the demonstration of the integrated performance of the NO_x emissions control systems and the SO_2 removal technologies. The results showed that a synergistic benefit occurred during the simultaneous operation of the SNCR and the sodium DSI system in that the NH_3 slip from the SNCR process suppressed the NO_2 emissions associated with NO to NO_2 oxidation by dry sodium injection.

Four series of air toxic tests were completed. Results indicated that the fabric filter successfully removed nearly all trace metal emissions and nearly 80% of the mercury emissions. Radionuclides, semi-volatile organic compounds, and dioxins/furans were below or very near their detectable limits.

Operating Performance

The Arapahoe Unit No. 4 operated more than 34,000 hours after combustion modifications were completed. The availability factor during the period was over 91%.

The operational test objectives were met or exceeded. However, there were operational lessons learned during the demonstration that will be useful in future deployment of the technologies. These "lessons learned" are summarized below.

It was found that control system modifications and additional operator training may be necessary to more accurately control NO_x reductions using low-NO_x burners under load-following conditions.

During the operation of the duct injection of calcium hydroxide and humidification under load-following conditions, fabric filter pressure-drop significantly increased. This was caused by the buildup of a hard ash cake on the fabric filter bags that could not be cleaned under normal reverse-air cleaning. The heavy ash cake was caused by the humidification system, but it was not determined whether the problem was due to operation at 30 ºF approach-to-saturation temperature or an excursion caused by a rapid decrease in load.

The performance of the ARIL lances in NO_x removal was good; however, the location created some operational problems. A large differential heating pattern between the top and bottom of the lance caused a significant amount of thermal expansion along the upper surface of the lance. This caused the lance to bend downwards approximately 12–18 inches after 30 minutes of exposure. Eventually the lances become permanently bent, thus making insertion and retraction difficult. The problem was partially resolved by adding cooling slots at the end of the lance. An alternative lance design provided by Diamond Power Specialty Company (a division of Babcock & Wilcox) was tested and found to have less bending due to evaporative cooling, even though its NO_x reduction and NH_3 slip performance were slightly less than for the ARIL lance.

When the SNCR and dry sodium systems were operated concurrently, an NH_3 odor problem was encountered around the ash silo. Reducing the NH_3 slip set points to the range of 4–5 ppm reduced the ammonia concentration in the fly ash to the 100–200 ppm range but the odor persisted. It was found that the problem was related to the rapid change in pH due to the presence of sodium in the ash. The rapid development of the high pH level and the attendant release of the ammonia vapor appear to be related to the wetting of the fly ash necessary to minimize fugitive dust emissions during transportation and handling. Handling ash in dry transport trucks solved this problem.

Economic Performance

Economic analysis is under way.

Commercial Applications

Either the entire Integrated Dry NO_x/SO_2 Emissions Control System or the individual technologies are applicable to most utility and industrial coal-fired units and provide lower capital-cost alternatives to conventional wet flue gas desulfurization processes. They can be retrofitted with modest capital investment and downtime, and their space requirements are substantially less. They can be applied to any unit size but are mostly applicable to the older, small- to mid-size units.

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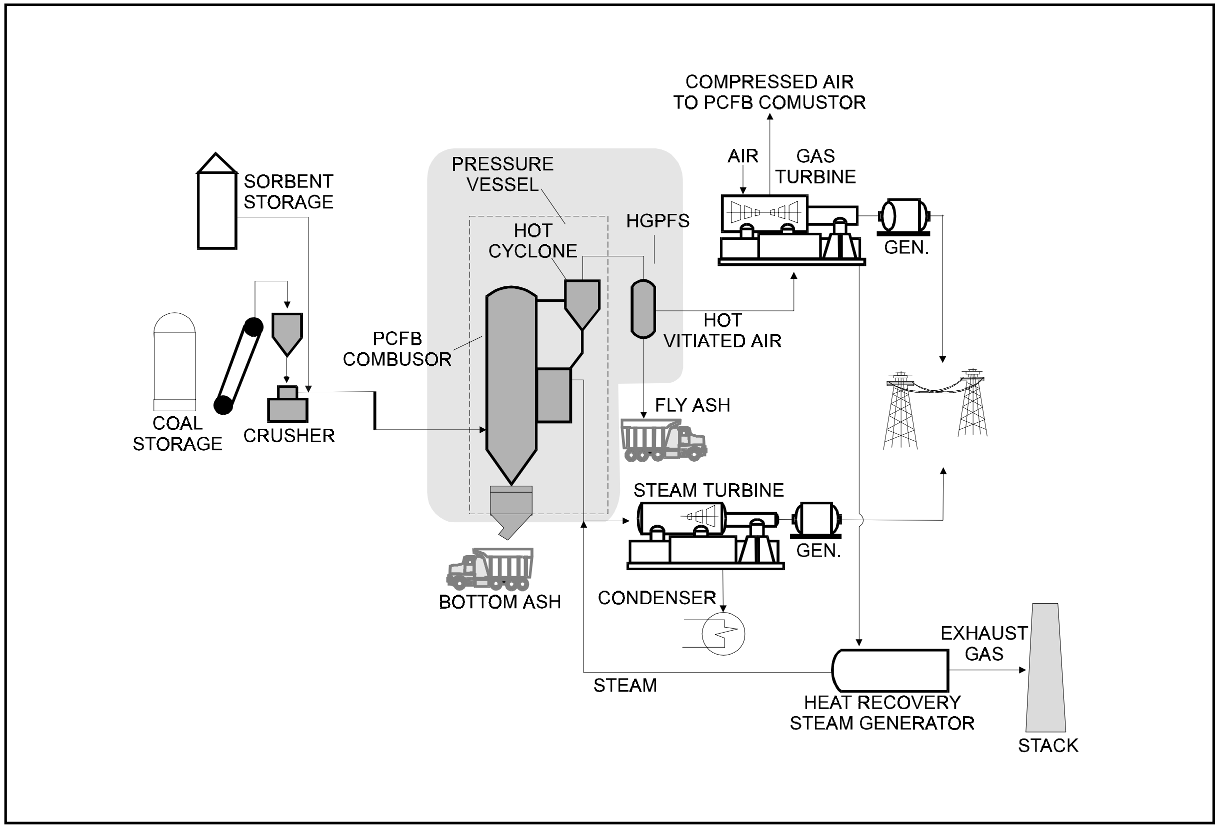
References

- Hunt, Terry, *et al.* "Integrated Dry NO_x/SO_2 Emissions Control System: Performance Summary." *Fifth Annual Clean Coal Technology Conference: Technical Papers*. January 1997.
- *Integrated Dry NO_x/SO_2 Emissions Control System Calcium-Based Dry Sorbent Injection: Test Report, April 30–November 2, 1993*. Report No. DOE/PC/90550-T14. Fossil Energy Research Corporation and Public Service Company of Colorado. December 1994. (Available from NTIS as DE95007932.)
- *Comprehensive Report to Congress on the Clean Coal Technology Program: Integrated Dry NO_x/SO_2 Emission Control System.* Public Service Company of Colorado. Report No. DOE/FE-0212P. U.S. Department of Energy. January 1991. (Available from NTIS as DE91008624.)

Advanced Electric Power Generation
Fluidized-Bed Combustion

McIntosh Unit 4A PCFB Demonstration Project



Participant
City of Lakeland, Lakeland Electric

Additional Team Members
Foster Wheeler Energy Corporation—supplier of pressurized circulating fluidized-bed (PCFB) combustor and heat exchanger and engineer

Siemens Westinghouse Power Corporation—supplier of hot gas filter, gas turbine, and steam turbine

Location
Lakeland, Polk County, FL (Lakeland's McIntosh Power Station, Unit No. 4)

Technology
Foster Wheeler's PCFB technology integrated with Siemens Westinghouse's hot gas particulate filter system (HGPFS) and power generation technologies

Plant Capacity/Production
145-MWe (net)

Project Funding

Total project cost	$186,588,000	100%
DOE	93,252,864	50
Participant	93,335,136	50

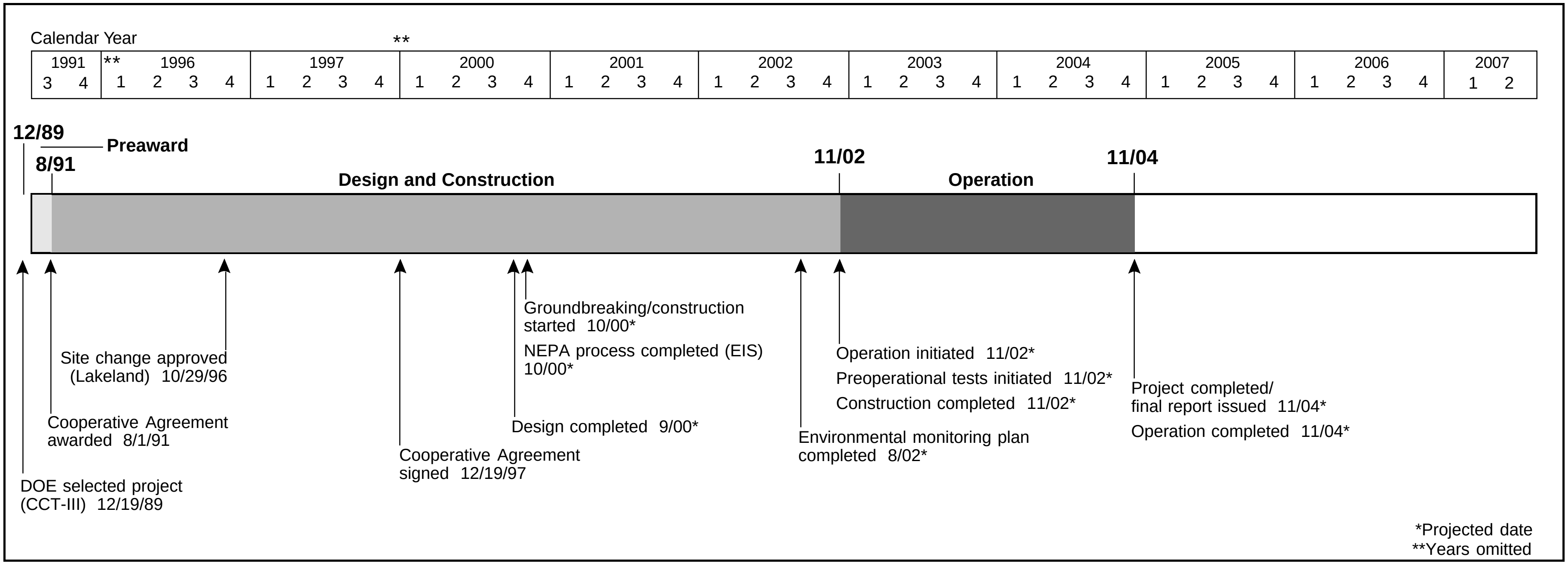
Project Objective
To demonstrate Foster Wheeler's PCFB technology coupled with Siemans Westinghouse's ceramic candle type hot gas filter and power generation technologies, which represent a cost-effective, high-efficiency, low-emissions means of adding generating capacity at greenfield sites or in repowering applications.

Technology/Project Description
The project resulted from a restructuring of the DMEC-1 PCFB Demonstration Project awarded under the third solicitation. In the first of the two Lakeland projects, McIntosh Unit No. 4 is being constructed with a PCFB combustor adjacent to the existing Unit No. 3. In the second project, the integration of a gasifier and topping combustor (topping cycle) with the PCFB technology will be demonstrated (see McIntosh Unit 4B Topped PCFB Demonstration Project).

Coal and limestone are mixed and fed into the combustion chamber. Combustion takes place at approximately 1,560–1,600 °F at a pressure of about 200 psig. The resulting flue gas and fly ash leaving the combustor pass through a cyclone and ceramic candle type HGPFS where the particulates are removed. The hot gas leaving the HGPFS is expanded through a gas turbine, which is based on a Siemens V64.3 gas turbine. The gas inlet temperature of less than 1,650 °F allows for a simplified turbine shaft and blade-cooling system. The hot gas leaving the gas turbine passes through a heat recovery unit used to generate steam. Heat recovered from both the combustor and heat recovery unit is used to generate steam to power a reheat steam turbine. Approximately 5–10% of the gross power is derived from the gas turbine, with the steam turbine contributing the balance.

The unit is being designed to burn a range of coals, including the current Eastern Kentucky coal burned in Unit No. 3 and high-ash, high-sulfur coals that are expected to be available at a lower cost. Limestone will be purchased from nearby Florida quarries. Ash will be disposed of in landfills or sold.

The project also includes a 104-MWe spare atmospheric fluidized-bed unit that can be fired on coal or char from the carbonizer and will replace the PCFB unit



during times of PCFB unavailability, allowing various modes of operation.

Project Status/Accomplishments

On December 19, 1997, a Cooperative Agreement modification was signed implementing the project restructuring from DMEC-1 to the City of Lakeland. The Lakeland City Council gave approval for the 10 year plan of Lakeland Electric (formerly Department of Electric & Water Utilities), which included this project, in September 1997. The project schedule anticipates the start of commercial operation of the PCFB (McIntosh 4A) in the winter of 2002. In parallel with the first two years of operation of the PCFB will be the design, fabrication, and construction of the topped PCFB technology (McIntosh 4B), with a planned start of operation in late 2004.

Negotiations continue between Lakeland and Foster Wheeler on the Engineer-Procure-Construct (EPC) proposal for the technology island.

Recent efforts focused on testing of the HGPFS, which is critical to system performance. Silicon carbide candle filters proved effective under conditions simulating those of the demonstration unit. At both 1,550 ºF and 1,400 ºF, the candle filters performed for over 1,000 hours at design levels without evidence of ash bridging or structural failure. Three new oxide-based candle filters showed promise as well. These will undergo further testing because of the potential for reduced cost and operation at higher temperatures.

Commercial Applications

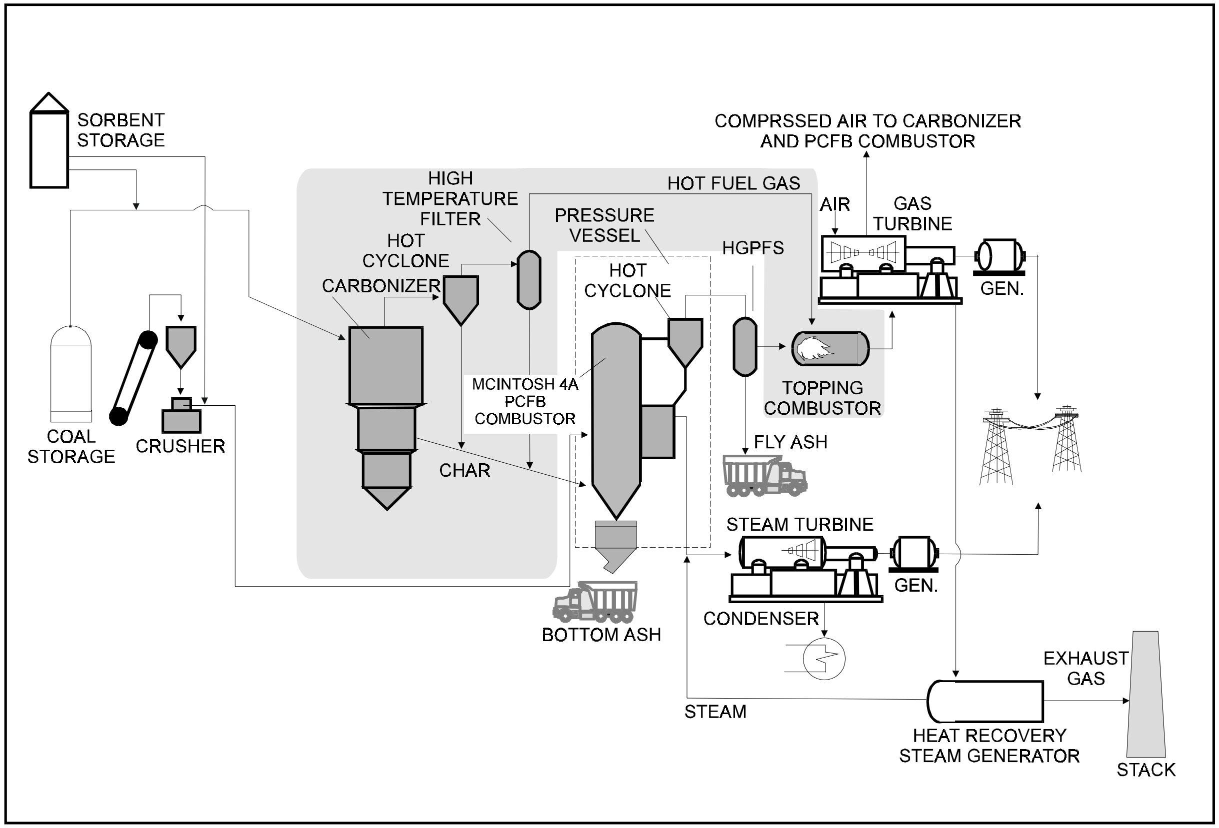
The project serves as a stepping stone to move the PCFB technology to readiness for widespread commercial deployment in the post-2000 time frame. The project will include the first commercial applications of hot gas particulate cleanup and one of the first to use a non-ruggedized gas turbine in a pressurized fluidized-bed application.

The combined-cycle PCFB system permits the combustion of a wide range of coals, including high-sulfur coals, and would compete with the pressurized bubbling-bed fluidized-bed system. PCFB can be used to repower or replace conventional power plants. Because of modular construction capability, PCFB generating plants permit utilities to add economical increments of capacity to match load growth or to repower plants using existing coal- and waste-handling equipment and steam turbines. Another advantage for repowering applications is the compactness of the process due to pressurized operation, which reduces space requirements per unit of energy generated.

The projected net heat rate for the system is approximately 9,511 Btu/kWh (based on HHV), which equates to over 35% efficiency.

Environmental attributes include in-situ sulfur removal of 95%, NO_x emissions less than 0.3 lb/10^6 Btu, and particulate matter discharge less than 0.03 lb/10^6 Btu. Solid waste will increase slightly as compared to conventional systems, but the dry material is readily disposable or potentially usable.

McIntosh Unit 4B Topped PCFB Demonstration Project



Participant

City of Lakeland, Lakeland Electric

Additional Team Members

Foster Wheeler Energy Corporation—supplier of carbonizer; engineer

Siemens Westinghouse Power Corporation—supplier of topping combustor and high-temperature filter

Location

Lakeland, Polk County, FL (Lakeland's McIntosh Power Station, Unit No. 4)

Technology

Fully integrated second-generation PCFB technology with the addition of a carbonizer island that includes Siemens Westinghouse's multi-annular swirl-burner (MASB) topping combustor

Plant Capacity/Production

93-MWe (net) addition to the 145-MWe (net) McIntosh 4A project

Project Funding

Total project cost	$219,635,546	100%
DOE	109,608,507	50
Participant	110,027,039	50

Project Objective

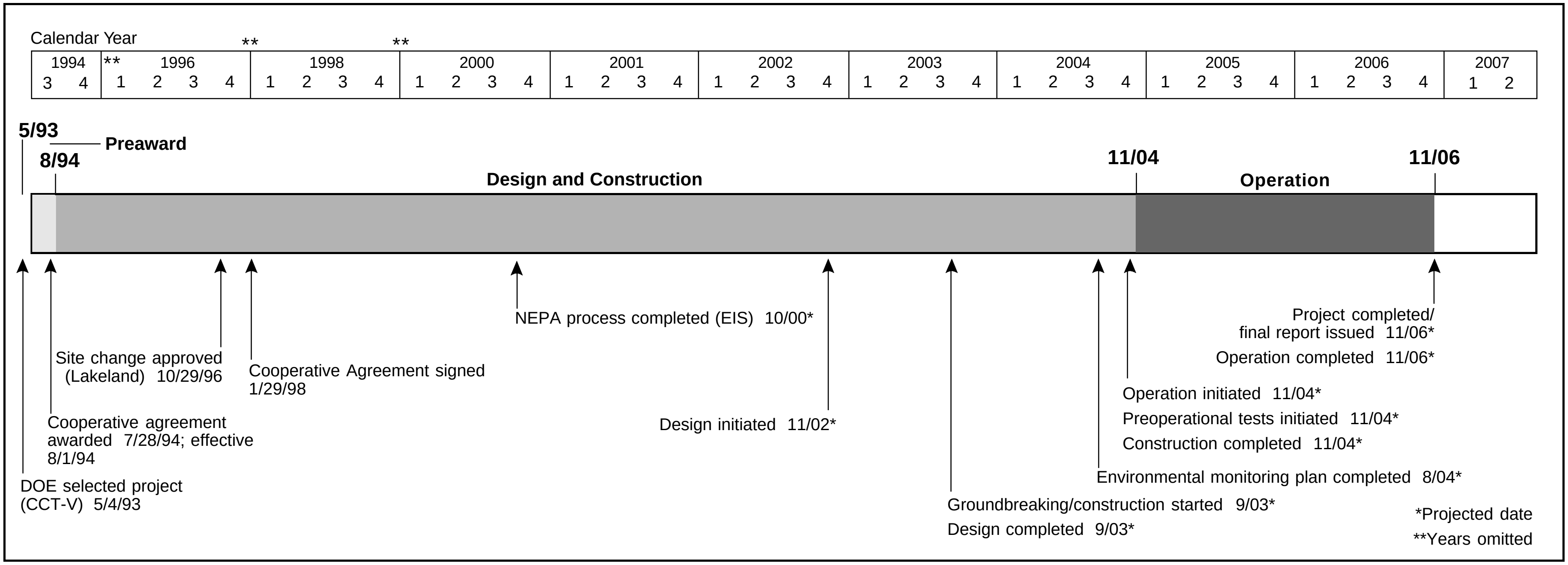
To demonstrate topped PCFB technology in a fully commercial power generating setting, thereby advancing the technology for future plants that will operate at higher gas turbine inlet temperatures and that are expected to achieve cycle efficiencies in excess of 45%.

Technology/Project Description

The project resulted from a restructuring of the Four Rivers Energy Modernization Project awarded under the fifth solicitation. The Four Rivers project was to demonstrate the integration of a gasifier and topping combustor (topping cycle) with the PCFB technology. By using a phased approach, Lakeland will be able to demonstrate both PCFB (McIntosh 4A) and topped PCFB (McIntosh 4B) technologies in a repowering application.

The project involves the addition of a carbonizer island to the PCFB demonstrated in the McIntosh 4A project. Dried coal and limestone are fed via a lock hopper system to the carbonizer together with part of the gas turbine discharge air. The coal is partially gasified at about 1,700 °F to produce syngas and char solids streams. The limestone is used to absorb sulfur compounds generated during the mild gasification process. After cooling the syngas to about 1,200 °F, the char and limestone entrained with the syngas are removed by a hot gas filter. The char and limestone are then transferred to the PCFB combustor for complete carbon combustion and limestone utilization. The hot, cleaned, filtered syngas is then fired in the MASB topping combustor to raise the turbine inlet temperature to approximately 2,400 °F. The gas is expanded through the turbine, cooled in a heat recovery unit, and exhausted to the stack. The net impact of the addition of the topping cycle is an increase in power output of 93-MWe and an associated improvement in plant heat rate of approximately 735 Btu/kWh. The coal and limestone used in McIntosh 4B are the same as those used in McIntosh 4A.

The 238-MWe plant is expected to have a heat rate



of 8,776 Btu/kWh (38.9% efficiency-HHV). Sulfur dioxide capture efficiency rate is 95%. Particulate and NO_x emissions are expected to be 0.02 lb/10^6 Btu and 0.17 lb/10^6 Btu, respectively. In the final configuration, the gas turbine will produce 57-MWe and the steam turbine will produce 181-MWe

Project Status/Accomplishments

On January 29, 1998, a Cooperative Agreement modification was signed implementing the project restructuring from Four Rivers Energy Partners to the City of Lakeland. The Lakeland City Council gave approval for the 10 year plan of Lakeland Electric (formerly Department of Electric & Water Utilities), which included this project, in September 1997. The project schedule anticipates the start of commercial operation of the PCFB (McIntosh 4A) in the winter of 2002. In parallel with the first two years of operation of the PCFB will be the design, fabrication, and construction of the topped PCFB technology (McIntosh 4B), with a planned start of operation in late 2004.

Negotiations continue between Lakeland and Foster Wheeler on the Engineer-Pressure-Construct (EPC) proposal for the technology island.

Recent efforts focused on testing of the HGPFS, which is critical to system performance. Silicon carbide and alumina/mullite candle filters proved effective under conditions simulating those of the demonstration unit. At both 1,550 ºF and 1,400 ºF, the candle filters performed for over 1,000 hours at design levels without evidence of ash bridging or structural failure. Three new oxide-based candle filters showed promise as well. These will undergo further testing because of the potential for reduced cost and operation at higher temperatures.

Commercial Applications

The commercial version of the topped PCFB technology will have a greenfield net plant efficiency of 45% (which equates to a heat rate approaching 7,500 Btu/kWh, based on HHV). In addition to higher plant efficiencies, the plant will (1) have a cost of electricity that is projected to be 20% lower than that of a conventional pulverized-coal-fired plant with flue gas desulfurization, (2) meet emission limits that are half those allowed by NSPS, (3) operate economically on a wide range of coals, and (4) be amenable to shop fabrication.

The benefits of improved efficiency include reduced cost for fuels and a reduction in CO_2 emissions. Other environmental attributes include in-situ sulfur retention that can meet 95% removal, NO_x emission that will be lower than 0.3 lb/10^6 Btu, and particulate matter dis-

JEA Large-Scale CFB Combustion Demonstration Project

Participant
JEA

Additional Team Member
Foster Wheeler Energy Corporation—co-owner and technology supplier

Location
Jacksonville, Duval County, FL (JEA's Northside Station, Unit No. 2)

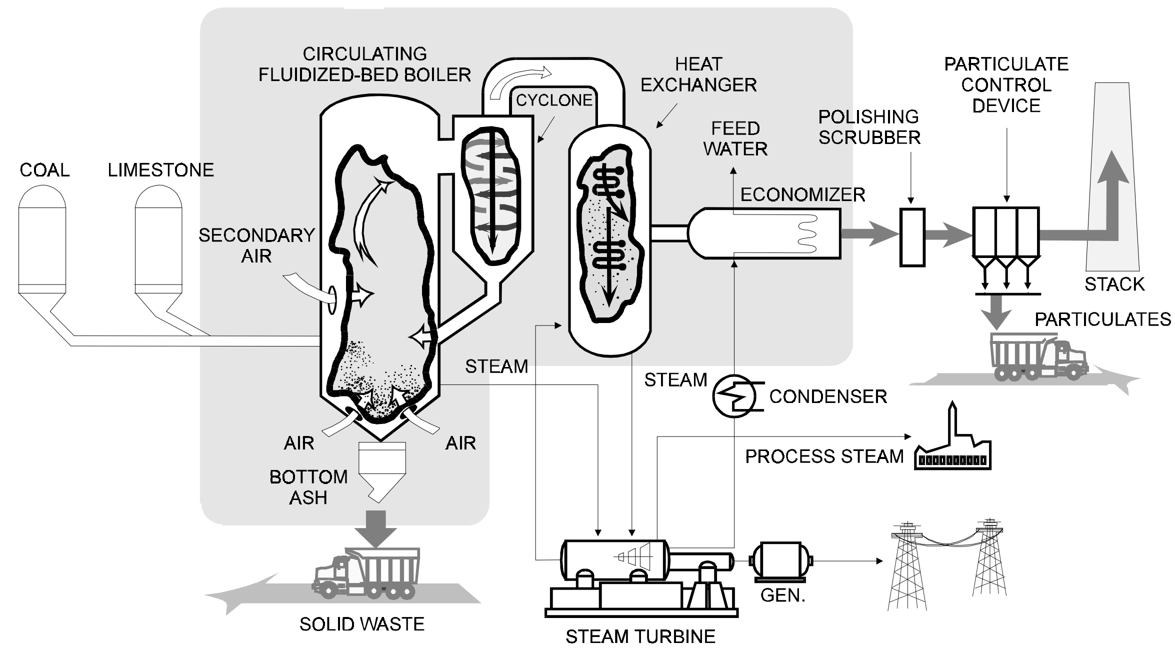
Technology
Foster Wheeler's atmospheric circulating fluidized-bed (ACFB) combustor

Plant Capacity/Production
297.5-MWe (gross), 265-MWe (net)

Project Funding

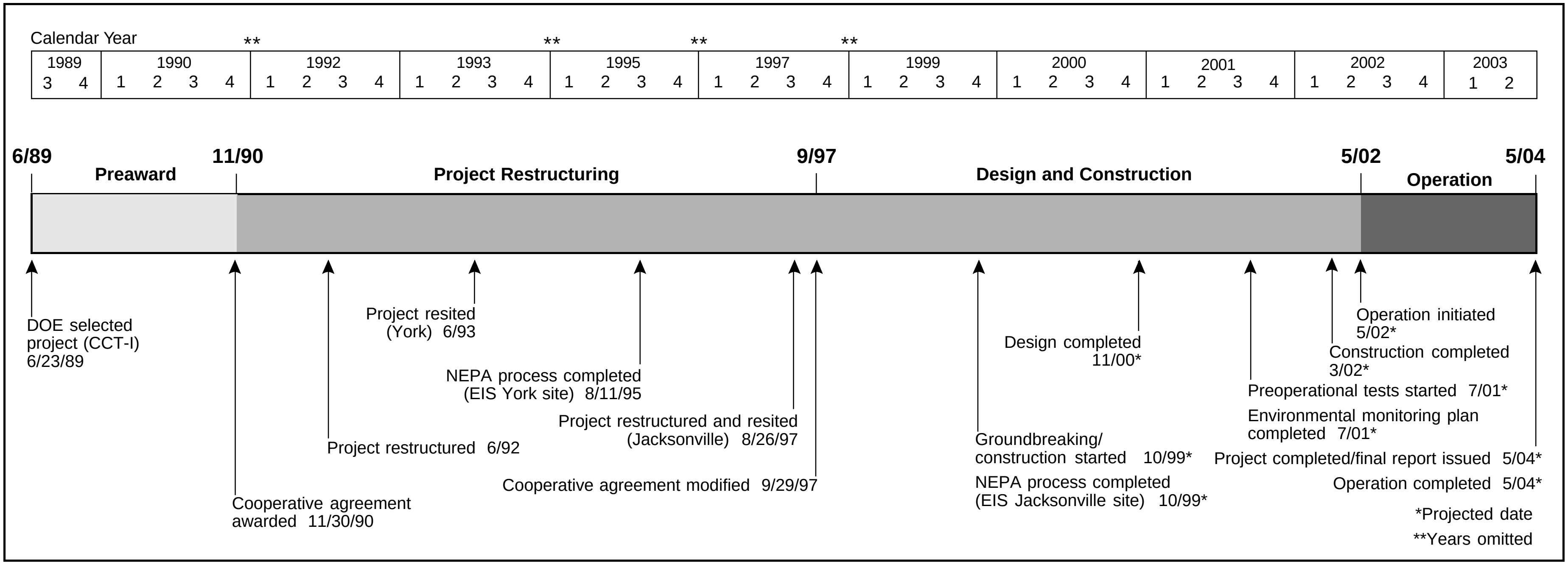
Total project cost	$309,096,512	100%
DOE	74,733,633	24
Participant	234,362,679	76

Project Objective
To demonstrate ACFB at 297.5-MWe gross (265-MWe net) representing a scale-up from previously constructed facilities; to verify expectations of the technology's economic, environmental, and technical performance to provide potential users with the data necessary for evaluating a large-scale ACFB as a commercial alternative; to accomplish greater than 90% SO_2 removal; and to reduce NO_x emissions by 60% when compared with conventional technology.



Technology/Project Description
A circulating fluidized-bed combustor, operating at atmospheric pressure, will be retrofitted into Unit No. 2 of the Northside Station. Coal or the secondary fuel, petroleum coke, primary air, and a solid sorbent, such as limestone, are introduced into the lower part of the combustor where initial combustion occurs. As the coal particles decrease in size due to combustion, they are carried higher in the combustor when secondary air is introduced. As the coal particles continue to be reduced in size, the coal, along with some of the sorbent, is carried out of the combustor, collected in a particle separator, and recycled to the lower portion of the combustor. Primary sulfur capture is achieved by limestone sorbent in the bed. However, additional SO_2 capture is achieved through the use of a polishing scrubber to be installed ahead of the particulate control equipment.

Steam is generated in tubes placed along the combustor's walls and superheated in tube bundles placed downstream of the particulate separator to protect against erosion. The system will produce approximately 2 x10^6 lb/hr of main steam at about 2,400 psig and 1,005 ºF and 1.73 x 10^6 lb/hr of reheat steam at 600 psig and 1,005 ºF. The steam will be used in an existing 297.5-MWe (nameplate) steam turbine and its generator. The heat rate for the retrofit plant is expected to be approximately 9,950 Btu/kWh (34% efficiency).



Project Status/Accomplishments

The project was successfully resited to Jacksonville after York County Energy partners and Metropolitan Edison Company terminated activities on the ACFB in September 1996. On August 26, 1997, DOE approved the transfer of the ACFB clean coal project from York, PA, to Jacksonville, FL. On September 29, 1997, DOE signed a modified cooperative agreement with JEA to cost-share refurbishment of the first (Unit No. 2) of two units at Northside Generating Station.

A Public Scoping Meeting on the Environmental Impact Statement (EIS) was held on December 3, 1997 at the Northside Station. The draft EIS is being prepared and will be submitted for review in March 1999.

The project, currently in design, moves atmospheric fluidized-bed combustion technology to the larger sizes of utility boilers being considered in capacity additions and replacements. The nominal 300-MWe demonstration unit in the JEA project will be more than double the size of the Nucla unit (110-MWe). Features include an integrated recycle heat exchanger (INTREX™) in the furnace, steam-cooled cyclones, a parallel pass reheat control, an SO_2 polishing scrubber, and a fabric filter for particulate control. Expected environmental performance is 0.17 lb/10^6 Btu SO_2 (98% reduction), 0.011 lb/10^6 Btu NO_x, and 0.017 lb/10^6 Btu particulates (0.013 lb/10^6 Btu PM_{10}).

Commercial Applications

ACFB technology has good potential for application in both the industrial and utility sectors, whether for use in repowering existing plants or in new facilities. ACFB is attractive for both baseload and dispatchable power applications because it can be efficiently turned down to 25% of full load. Coal of any sulfur or ash content can be used, and any type or size of a coal-fired boiler can be repowered. In repowering applications, an existing plant area is used, and coal- and waste-handling equipment as well as steam turbine equipment are retained, thereby extending the life of a plant.

In its commercial configuration, ACFB technology offers several potential benefits when compared to conventional pulverized coal-fired systems: lower capital costs; reduced SO_2 and NO_x emissions at lower costs; higher combustion efficiency; and dry, granular solid material that is easily disposed of or potentially

Tidd PFBC Demonstration Project

Project completed.

Participant
The Ohio Power Company

Additional Team Members
American Electric Power Service Corporation—designer, constructor, and manager
The Babcock & Wilcox Company—technology supplier
Ohio Coal Development Office—cofunder

Location
Brilliant, Jefferson County, OH (Ohio Power Company's Tidd Plant, Unit No. 1)

Technology
The Babcock & Wilcox Company's pressurized fluidized-bed combustion (PFBC) system (under license from ABB Carbon)

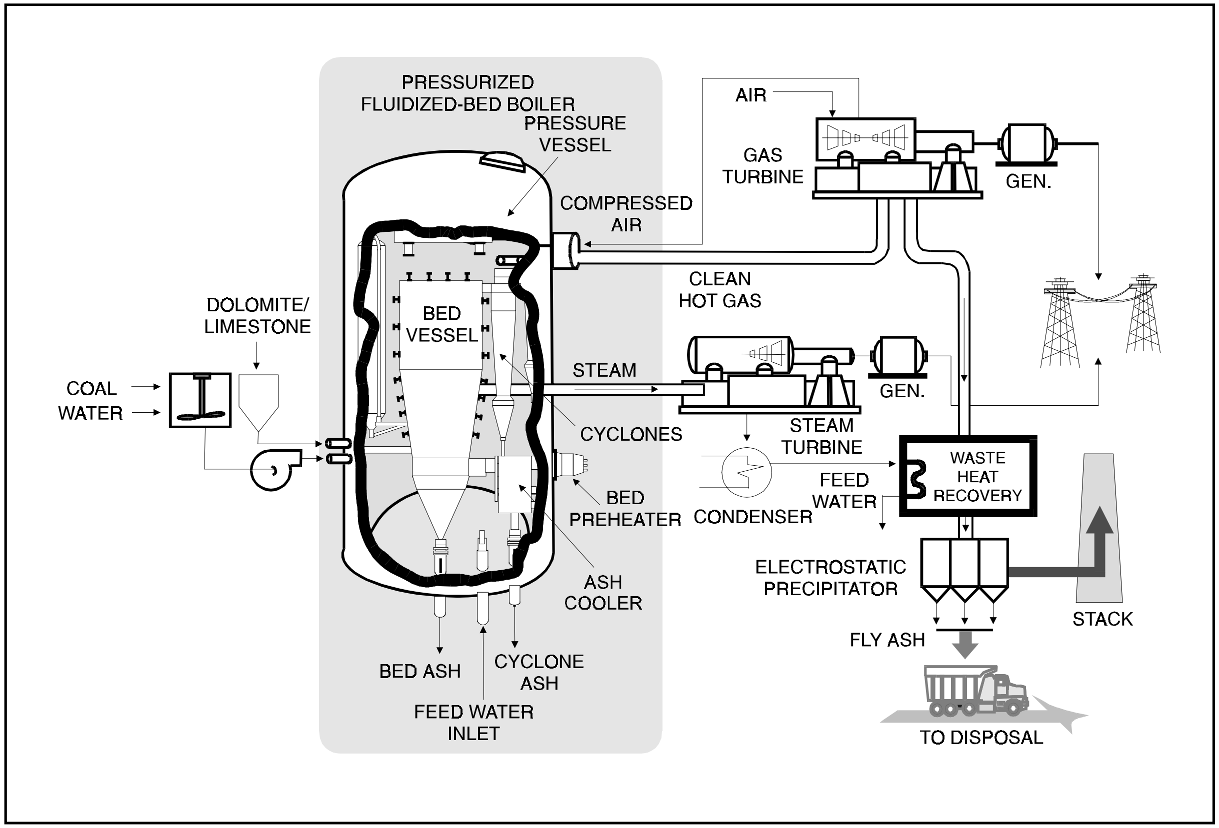
Plant Capacity/Production
70-MWe

Coal
Ohio bituminous, 2–4% sulfur

Project Funding

Total project cost	$189,886,339	100%
DOE	66,956,993	35
Participant	122,929,346	65

Project Objective
To verify expectations of PFBC economic, environmental, and technical performance in a combined-cycle repowering application at utility scale; and to accomplish greater than 90% SO_2 removal and NO_x emission level of 0.2 lb/10^6 Btu at full load.

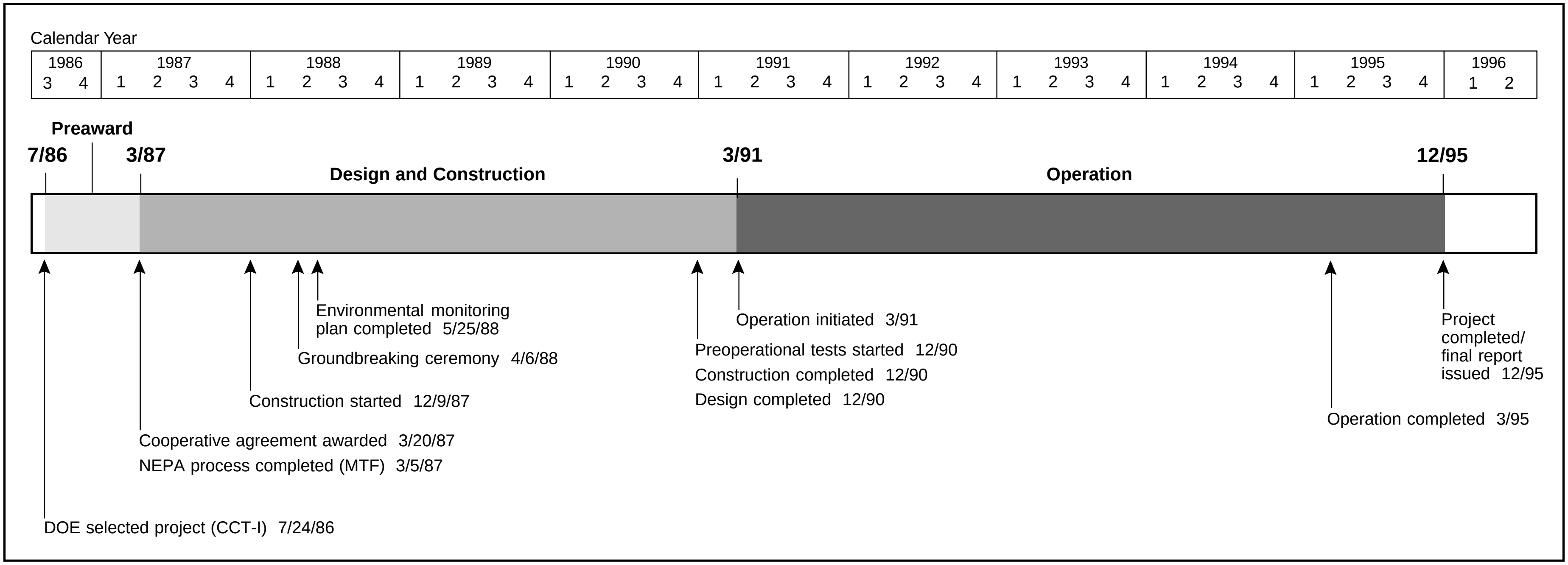


Technology/Project Description
Tidd was the first large-scale operational demonstration of PFBC in the United States and one of only five worldwide. The project represented a 13:1 scaleup from the pilot facility.

The boiler, cyclones, bed reinjection vessels, and associated hardware were encapsulated in a pressure vessel 45 feet in diameter and 70 feet high. The facility was designed so that one-seventh of the hot gases produced could be routed to an Advanced Particulate Filter (APF).

The Tidd facility is a bubbling fluidized-bed combustion process operating at 12 atm (175 psi). Pressurized combustion air is supplied by the turbine compressor to fluidize the bed material, which consists of a coal-water fuel paste, coal ash, and a dolomite or limestone sorbent. Dolomite or limestone in the bed reacts with sulfur to form calcium sulfate, a dry, granular bed-ash material, which is easily disposed of or is usable as a by-product. A low bed-temperature of about 1,600 ºF limits NO_x formation.

The hot combustion gases exit the bed vessel with entrained ash particles, 98% of which are removed when the gases pass through cyclones. The cleaned gases are then expanded through a 15-MWe gas turbine. Heat from the gases exiting the turbine, combined with heat from a tube bundle in the fluid bed, generates steam to drive an existing 55-MWe steam turbine.



Results Summary

Environmental

- Sorbent size had the greatest effect on SO_2 removal efficiency as well as stabilization and heat transfer characteristics of the fluidized-bed.
- SO_2 removal efficiency of 90% was achieved at full load with a calcium-to-sulfur (Ca/S) molar ratio of 1.14 and temperature of 1,580 ºF.
- SO_2 removal efficiency of 95% was achieved at full load with a Ca/S molar ratio of 1.5 and temperature of 1,580 ºF.
- NO_x emissions were 0.15–0.33 lb/10^6 Btu.
- CO emissions were less than 0.01 lb/10^6 Btu.
- Particulate emissions were less than 0.02 lb/10^6 Btu.

Operational

- Combustion efficiency ranged from an average 99.3% at low bed levels to an average 99.5% at moderate to full bed levels.
- Heat rate was 10,280 Btu/kWh (HHV-grass output) (33.2% efficiency) because the unit was small and no attempt was made to optimize heat recovery.
- An Advanced Particulate Filter (APF), using a silicon carbide candle filter array, achieved 99.99% filtration efficiency on a mass basis.
- PFBC boiler demonstrated commercial readiness.
- ASEA Stal GT-35P gas turbine proved capable of operating commercially in a PFBC flue gas environment.

Economic

- The Tidd plant was a relatively small-scale facility, as such, detailed economics were not prepared as part of this project.
- A recent cost estimate performed on Japan's 360-MWe PFBC Karita Plant, due to commence operation in 1999, projected a capital cost of $1,263/kW (1997$).

Project Summary

The Tidd PFBC technology is a bubbling fluidized-bed combustion process operating at 12 atmospheres (175 psi). Fluidized combustion is inherently efficient. A pressurized environment further enhances combustion efficiency, allowing very low temperatures that mitigate thermal NO_x generation, flue gas/sorbent reactions that increase sorbent utilization, and flue gas energy that is used to drive a gas turbine. The latter contributed significantly to system efficiency because of the high efficiency of gas turbines and the availability of gas turbine exhaust heat that can be applied to the steam cycle. A bed design temperature of 1,580 ºF was established because it was the maximum allowable temperature at the gas turbine inlet and was well below temperatures for coal ash fusion, thermal NO_x formation, and alkali vaporization.

Coal crushed to ¼ inch or less was injected into the combustor as a coal/water paste containing 25% water by weight. Crushed sorbent, either dolomite or limestone, was injected into the fluidized bed via two pneumatic feed lines, supplied from two lock hoppers. The sorbent feed system initially used two injector nozzles but was modified to add two more for nozzles to enhance distribution.

In 1992, a 10-MWe equivalent APF was installed and commissioned as part of a research and development program and not part of the CCT demonstration. This system used ceramic candle filters to clean one-seventh of the exhaust gases from the PFBC system. The hot gas cleanup system unit replaced one of the seven secondary cyclones.

The Tidd PFBC demonstration plant accumulated 11,444 hours of coal-fired operations during its 54 months of operation. The unit completed 95 parametric tests, including continuous coal-fired runs of 28, 29, 30, 31, and 45 days. Ohio bituminous coals having sulfur contents of 2–4% were used in the demonstration.

Environmental Performance

Testing showed that 90% SO_2 capture was achievable with a Ca/S molar ratio of 1.14 and that 95% SO_2 capture was possible with a Ca/S molar ratio of 1.5, provided the size gradation of the sorbent being utilized was optimized. This sulfur retention was achieved at a bed temperature of 1,580 ºF and full bed height. Limestone deterioration of the fluidized-bed, and as a result, testing focused on dolomite. The testing showed that sulfur capture as well as sintering was sensitive to the fineness of the dolomite sorbent (Plum Run Greenfield dolomite was the design sorbent). Sintering of fluidized-bed materials, a fusing of the materials rather than effective reaction, had become a serious problem that required operation at bed temperatures below the optimum for effective boiler operation. Tests were conducted with sorbent size reduced from minus 6 mesh to a minus 12 mesh. The result with the finer material was a major, positive impact on process performance without the expected excessive elutriation of sorbent. The finer material increased the fluidization activity as evidenced by a 10% improvement in heat transfer rate and an approximately 30% increase in sorbent utilization. In addition, the process was much more stable as indicated by reductions in temperature variations in both the bed and the evaporator tubes. Further, sintering was effectively eliminated.

NO_x emissions ranged from 0.15–0.33 lb/10^6 Btu, but were typically 0.2 lb/10^6 Btu during the demonstration. These emissions were inherent to the process, which was operating at approximately 1,580 ºF. No NO_x control enhancements, such as ammonia injection, were required. Emissions of carbon monoxide and particulates were less than 0.01 and 0.02 lb/10^6 Btu, respectively.

Operational Performance

Except for localized erosion of the in-bed tube bundle and the more general erosion of the water walls, the Tidd boiler performed extremely well and was considered a commercially viable design. The in-bed tube bundle experienced no widespread erosion that would require significant maintenance. While the tube bundle experienced little wear, a significant amount of erosion on each of the four water walls was observed. This erosion posed no problem, however, because the area affected is not critical to heat transfer and could be protected by refractory.

The prototype gas turbine experienced structural problems and was the leading cause of unit unavailability during the first 3 years of operation. However, design changes instituted over the course of the demonstration proved effective in addressing the problem. The Tidd demonstration showed that a gas turbine could operate in a PFBC flue gas environment.

Efficiency of the PFBC combustion process was calculated during testing from the amount of unburned carbon in cyclone and bed ash, together with measurements of the amount of carbon monoxide in the flue gas. Combustion efficiencies averaged 99.5% at moderate to full bed heights, surpassing the design or expected efficiency of 99.0%.

Using data for typical full-load operation, a heat rate of 10,280 Btu/kWh (HHV basis) was calculated. This corresponds to a cycle thermodynamic efficiency of 33.2% at a point where the cycle produced 70-MWe of gross electrical power while burning Pittsburgh No. 8 coal. Because the Tidd plant was a repowering application at a comparatively small scale, the measured efficiency does not represent what would be expected for a larger utility-scale plant using Tidd technology. Studies conducted under the PFBC Utility Demonstration Project showed that efficiencies of over 40% are likely for a larger utility-scale PFBC plant.

▲ The PFBC demonstration at the repowered 70-MWe unit at Ohio Power's Tidd Plant led to significant refinements and understanding of the technology.

In summary, the Tidd project showed that the PFBC system could be applied to electric power generation. Further, the demonstration project led to significant refinements and understanding of the technology in the areas of turbine design, sorbent utilization, sintering, post-bed combustion, ash removal, and boiler materials.

Testing of the APF for over 5,800 hours of coal-fired operation showed that the APF vessel was structurally adequate; the clay-bonded silicon carbide candle filters were structurally adequate unless subjected to side loads from ash bridging or build-up in the vessel; bridging was precluded with larger particulates included in the particulate matter; and filtration efficiency (mass basis) was 99.99%.

Economic Performance

The Tidd plant was a relatively small-scale facility, detailed economics were not prepared as part of this project. However, a recent cost estimate performed on Japan's 360-MWe PFBC Karita Plant, due to commence operation in 1999, projected a capital cost of $1,263/kW (1997$).

Commercial Applications

Combined-cycle PFBC permits use of a wide range of coals, including high-sulfur coals. The compactness of Bubbling PFBC technology allows utilities to significantly increase capacity at existing sites. PFBC technology appears to be best suited for applications of 50-MWe or larger. Capable of being constructed modularly, PFBC generating plants permit utilities to add increments of capacity economically to match load growth. Plant life can be extended by repowering with PFBC using the existing plant area, coal- and waste-handling equipment, and steam turbine equipment. Another advantage for repowering applications is the compactness of the process due to pressurized operation, which reduces space requirements per unit of energy generated.

The 360-MWe Kapita Plant in Japan, which will use ABB Carbon P800 technology, represents a major move toward commercialization of PFBC bubbling-bed technology. A second generation P200 PFBC is under construction in Germany. Other PFBC projects are under consideration in China, South Korea, the United Kingdom, Italy, and Israel.

The Tidd project received *Power* magazine's 1991 Powerplant Award. In 1992, the project received the National Energy Resource Organization award for demonstrating energy-efficient technology.

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References

- *Tidd PFBC Hot Gas Clean Up Program Final Report.* Report No. DOE/MC/26042-5130. The Ohio Power Company. October 1995. (Available from NTIS as DE96000650.)
- *Tidd PFBC Demonstration Project Final Report, Including Fourth Year of Operation.* The Ohio Power Company. August 1995. (Available from DOE Library/Morgantown, 1-800-432-8330, ext. 4184 as DE96000623.)
- *Tidd PFBC Demonstration Project Final Report, March 1, 1994–March 30, 1995.* Report No. DOE/MC/24132-T8. The Ohio Power Company. August 1995. (Available from NTIS as DE96004973.)
- *Tidd PFBC Demonstration Project—First Three Years of Operation.* Report No. DOE/MC/24132-5037-vol. 1 and 2. The Ohio Power Company. April 1995. (Available from NTIS as DE96000559 for vol. 1 and DE96003781 for vol. 2.)
- *A Study of Hazardous Air Pollutants at the Tidd PFBC Demonstration Plant.* Report No. DOE/MC/26042-4083. American Electric Power Service Corporation. October 1994. (Available from NTIS as DE95009729.)
- *Tidd PFBC Demonstration Project Topical Report—First Eighteen Months of Operation.* Report No. DOE/MC/24132-3746. The Ohio Power Company. March 1994. (Available from NTIS as DE94004120.)
- *Tidd PFBC Demonstration Project: Public Final Design Report.* Report No. DOE/MC/24132-3195. The Ohio Power Company. October 1992. (Available from NTIS as DE93000234.)
- *Comprehensive Report to Congress on the Clean Coal Technology Program: Tidd PFBC Demonstration Project*. The Ohio Power Company. Report No. DOE/FE-0078. U.S. Department of Energy. February 1987. (Available from NTIS as DE87005803.)

▲ Coal and sorbent conveyors can be seen just after entering the Tidd Plant.

Nucla CFB Demonstration Project

Project completed.

Participant

Tri-State Generation and Transmission Association, Inc. (formerly Colorado-Ute Electric Association, Inc.)

Additional Team Members

Foster Wheeler Energy Corporation*—technology supplier
Technical Advisory Group (potential users)—cofunder
Electric Power Research Institute—technical consultant

Location

Nucla, Montrose County, CO (Nucla Station)

Technology

Foster Wheeler's atmospheric circulating fluidized-bed (ACFB) combustion system

Plant Capacity/Production

100-MWe (net)

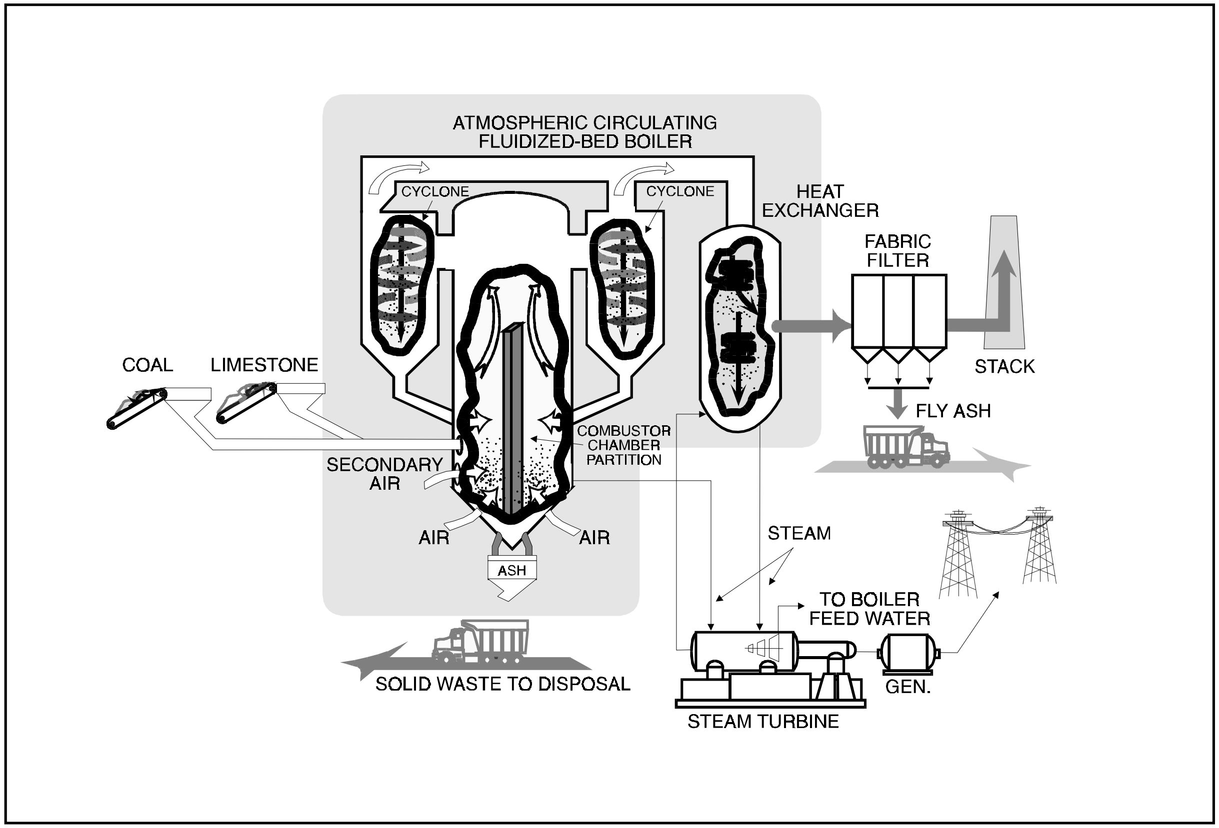
Coals

Western bituminous—
  Salt Creek, 0.5% sulfur, 17% ash
  Peabody, 0.7% sulfur, 18% ash
  Dorchester, 1.5% sulfur, 23% ash

Project Funding

Total project cost	$46,512,678	100%
DOE	17,130,411	37
Participant	29,382,267	63

*Pyropower Corporation, the original technology developer and supplier, was acquired by Foster Wheeler Energy Corp.



Project Objective

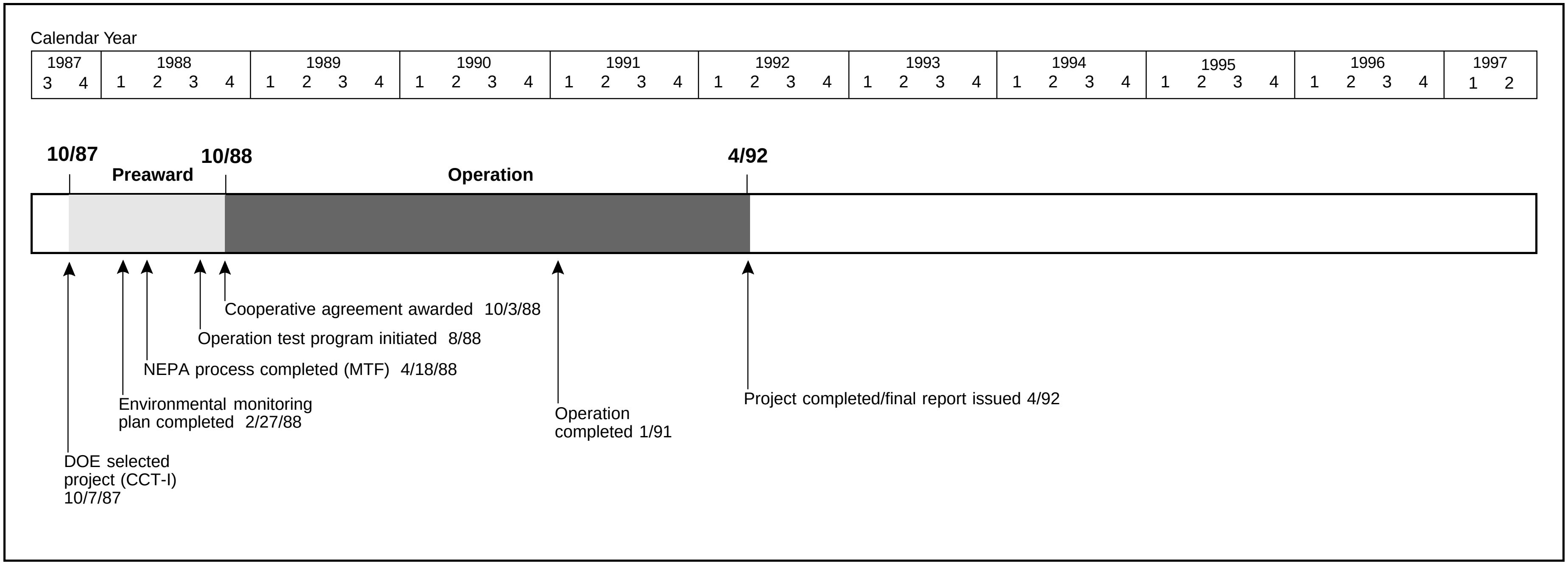
To demonstrate the feasibility of ACFB technology at utility scale and to evaluate the economic environmental, and operational performance at that scale.

Technology/Project Description

Nucla's circulating fluidized-bed system operates at atmospheric pressure. In the combustion chamber, a stream of air fluidizes and entrains a bed of coal, coal ash, and sorbent (e.g., limestone). Relatively low combustion temperatures limit NO_x formation. Calcium in the sorbent combines with SO_2 gas to form calcium sulfite and sulfate solids, and solids exit the combustion chamber and flow into a hot cyclone. The cyclone separates the solids from the gases, and the solids are recycled for combustor temperature control. Continuous circulation of coal and sorbent improves mixing and extends the contact time of solids and gases, thus promoting high utilization of the coal and high-sulfur-capture efficiency. Heat in the flue gas exiting the hot cyclone is recovered in the economizer. Flue gas passes through a baghouse where particulate matter is removed. Steam generated in the ACFB is used to produce electric power.

Three small, coal-fired, stoker-type boilers at Nucla Station were replaced with a new 925,000-lb/hr ACFB steam generator capable of driving a new 74-MWe turbine generator. Extraction steam from this turbine generator powers three existing turbine generators (12-MWe each).

In 1992, Colorado-Ute Electric Association, Inc., the owner of Nucla Station, was purchased by Tri-State Generation and Transmission Association, Inc.



Results Summary

Environmental

- Bed temperature had the greatest effect on pollutant emissions and boiler efficiency.
- At bed temperatures below 1,620 ºF, sulfur capture efficiencies of 70 and 95% were achieved at calcium-to-sulfur (Ca/S) molar ratios of 1.5 and 4.0, respectively.
- During all tests, NO_x emissions averaged 0.18 lb/10^6 Btu and did not exceed 0.34 lb/10^6 Btu.
- CO emissions ranged from 70–140 ppmv.
- Particulate emissions ranged from 0.0072–0.0125 lb/10^6 Btu, corresponding to a removal efficiency of 99.9%.
- Solid waste was essentially benign and showed potential as an agricultural soil amendment, soil/road bed stabilizer, or landfill cap.

Operational

- Boiler efficiency ranged from 85.6–88.6% and combustion efficiency ranged from 96.9–98.9%.
- A 3:1 boiler turndown capability was demonstrated.
- Heat rate at full load was 11,600 Btu/kWh and was 12,400 Btu/kWh at half load.

Economic

- Capital cost for the Nucla retrofit was $1,123/kW and a normalized power production cost was 64 mills/kWh.

Project Summary

Fluidized-bed combustion evolved from efforts to find a combustion process conducive to controlling pollutant emissions without external controls. Fluidized-bed combustion enables efficient combustion at temperatures of 1,400–1,700 ºF, well below the thermal-NO_x formation temperature (2,500 ºF), and high SO_2-capture efficiency through effective sorbent/flue gas contact. ACFB differs from the more traditional fluid-bed combustion. Rather than submerging a heat exchanger in the fluid bed, which dictates a low-fluidization velocity, ACFB uses a relatively high fluidization velocity, which entrains the bed material. Hot cyclones capture and return the solids emerging from the turbulent bed to control temperature and extend the gas/solid contact time and to protect a downstream heat exchanger.

Interest and participation of the Department of Energy, Electric Power Research Institute, and Technical Advisory Group (potential users) in the project involved evaluating ACFB potential for broad utility application through a comprehensive test program. Over a 2½-year period, 72 steady-state performance tests were conducted and 15,700 hours logged. The result was a database that remains the most comprehensive, available resource on ACFB technology.

Operational Performance

Between July 1988 and January 1991, the plant operated with an average availability of 58% and an average capacity factor of 40%. However, toward the end of the demonstration, most of the technical problems had been overcome. During the last three months of the demonstration, average availability was 97% and the capacity factor, 66.5%.

Over the range of operating temperature at which testing was performed, bed temperature was found to be the most influential operating parameter. With the exception of coal-fired configuration and excess air at elevated temperatures, bed temperature was the only parameter that had a measurable impact on emissions and efficiency.

Combustion efficiency, a measure of the quantity of carbon that is fully oxidized to CO_2, ranged from 96.9–98.9%. Of the four exit sources of incompletely burned carbon, the largest was carbon contained in the fly ash (93%). The next largest (5%) was carbon contained in the bottom ash stream, and the remaining feed-carbon loss (2%) was incompletely oxidized CO in the flue gas. The fourth possible source, hydrocarbons in the flue gas, was measured and found to be negligible.

Boiler efficiencies for 68 performance tests varied from 85.6–88.6%. The contributions to boiler heat loss were identified as unburned carbon, sensible heat in dry flue gas, fuel and sorbent moisture, latent heat in burning hydrogen, sorbent calcination, radiation and convection, and bottom-ash cooling water. Net plant heat rate decreased with increasing boiler load, from 12,400 Btu/kWh at 50% of full load to 11,600 Btu/kWh at full load. The lowest value achieved during a full-load steady-state test was 10,980 Btu/kWh. These values were affected by the absence of reheat, the presence of the three older 12.5-MWe turbines in the overall steam cycle, the number of unit restarts, and part-load testing.

Environmental Performance

As indicated above, bed temperature had the greatest impact on ACFB performance, including pollutant emissions. Exhibit 5-38 shows the effect of bed temperatures on the Ca/S molar ratio requirement for 70% sulfur retention. Ca/S molar ratios were calculated based on the calcium content of the sorbent only and do not account for the calcium content of the coal. While a Ca/S molar ratio of about 1.5 was sufficient to achieve 70% sulfur retention in the 1,500–1,620 °F range, the Ca/S molar ratio requirement jumped to 5.0 or more at 1,700 °F or greater.

Exhibit 5-39 shows the effect of Ca/S molar ratio on sulfur retention at average bed temperatures below 1,620 ºF. Salt Creek and Peabody coals contain 0.5% and 0.7% sulfur, respectively. To achieve 70% SO_2 reduction, or the 0.4 lb/10^6 Btu emission rate required by the licensing agreement, a Ca/S molar ratio of approximately 1.5 is required. To achieve an SO_2 reduction of 95%, a Ca/S molar ratio of approximately 4.0 is necessary. Dorchester coal, averaging 1.5% sulfur content, required a somewhat lower Ca/S molar ratio for a given retention.

NO_x emissions measured throughout the demonstration were less than 0.34 lb/10^6 Btu, which is well below the regulated value of 0.5 lb/10^6 Btu. The average level of NO_x emissions for all tests was 0.18 lb/10^6 Btu. NO_x emissions indicate a relatively strong correlation with temperature, increasing from 40 ppmv (0.06 lb/10^6 Btu) at 1,425 ºF to 240 ppmv (0.34 lb/10^6 Btu) at 1,700 °F. Limestone feed rate was also identified as a variable affecting NO_x emissions, i.e., somewhat higher NO_x emissions resulted from increasing calcium-to-nitrogen (Ca/N) molar ratios. The mechanism was believed to be oxidation of volatile nitrogen in the form of ammonia (NH_3) catalyzed by calcium oxide.

CO emissions decrease as temperature increases, from 140 ppmv at 1,425 ºF to 70 ppmv at 1,700 ºF.

At full load, the hot cyclones removed 99.8% of the particulates. With the addition of baghouses, removal efficiencies achieved

Exhibit 5-38
Effect of Bed Temperature on Ca/S Requirement

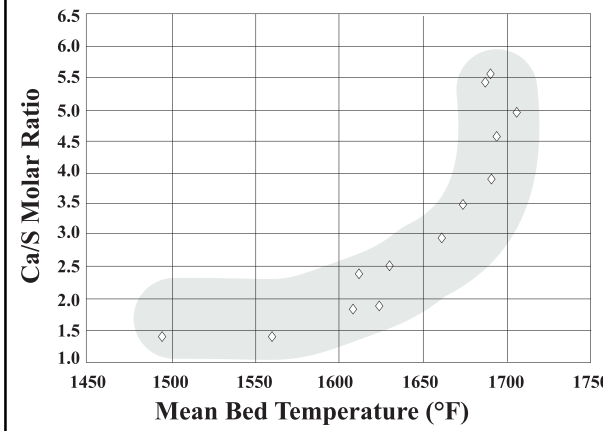
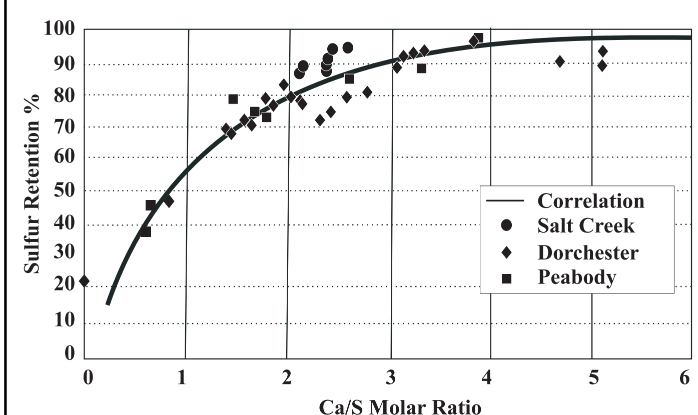


Exhibit 5-39
Calcium Requirements and Sulfur Retentions for Various Fuels



on Peabody and Salt Creek Coals were 99.905% and 99.959%, respectively. This equated to emission levels of 0.0125 lb/10^6 Btu for Peabody coal and 0.0072 lb/10^6 Btu for Salt Creek coal, well below the required 0.03 lb/10^6 Btu.

Economic Performance

The final capital costs associated with the engineering, construction, and start-up of the Nucla ACFB system were $112.3 million. This represents a cost of $1,123/kW (net). Total power costs associated with plant operations between September 1988 and January 1991 were approximately $54.7 million, resulting in a normalized cost of power production of 64 mills/kWh. The average monthly operating cost over this period was about $1,888,000. Fixed costs represent about 62% of the total and include interest (47%), taxes (4.8%), depreciation (6.9%), and insurance (2.7%). Variable costs represent more than 38% of the power production costs and include fuel expenses (26.2%), non-fuel expenses (6.8%), and maintenance expenses (5.5%).

▲ The 110-MWe Nucla ACFB demonstration enabled Pyropower Corporation (now owned by Foster Wheeler) to save almost 3 years in establishing a commercial line of ACFB units.

Commercial Applications

The Nucla project represented the first repowering of a U.S. utility plant with ACFB technology and showed the technology's effectiveness to burn a wide variety of coals cleanly and efficiently. The comprehensive database resulting from the Nucla project enabled the resultant technology to be replicated in numerous commercial plants throughout the world. Nucla continues in commercial service.

Today, every major boiler manufacturer offers an ACFB system in its product line. There are now more than 170 fluidized-bed combustion boilers of varying capacity operating in the U.S. and the technology has made significant market penetration abroad. The fuel flexibility and ease of operation make it a particularly attractive power generation option for the burgeoning power market in developing countries.

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References

- *Colorado-Ute Nucla Station Circulating Fluidized-Bed (CFB) Demonstration—Volume 2: Test Program Results.* EPRI Report No. GS-7483. October 1991.
- *Demonstration Program Performance Test: Summary Reports.* Report No. DOE/MC/25137-3104. Colorado-Ute Electric Association, Inc. March 1992. (Available from NTIS as DE92001299.)
- *Economic Evaluation Report: Topical Report.* Report No. DOE/MC/25137-3127. Colorado-Ute Electric Association, Inc., March 1992. (Available from NTIS as DE93000212.)
- *Nucla CFB Demonstration Project: Detailed Public Design Report.* Report No. DOE/MC/25137-2999. Colorado-Ute Electric Association, Inc., December 1990. (Available from NTIS as DE91002081.)
- *Clean Coal Reference Plants: Atmospheric CFB (Topical Report, Task 1).* Report No. DOE/MC/25177-3307. Gilbert/Commonwealth, Inc. June 1992. (Available from NTIS as DE93000251.)
- *Comprehensive Report to Congress on the Clean Coal Technology Program: Nucla CFB Demonstration Project.* (Colorado-Ute Electric Association, Inc.). Report No. DOE/FE-0106. U.S. Department of Energy. July 1988.

Advanced Electric Power Generation
Integrated Gasification Combined-Cycle

Clean Energy Demonstration Project

Participant
Clean Energy Partners Limited Partnership (a limited partnership consisting of Clean Energy Genco, Inc., an affiliate of Duke Energy Corp.; AMEREN Corporation and Energy Research Corporation)

Additional Team Members
Duke Engineering & Services, Inc.—engineer and constructor

General Electric Company—power island designer and supplier

British Gas Americas, Inc., in conjunction with Lurgi Energie and Umwelt GmbH—gasification island designer

Energy Research Corporation—molten carbonate fuel cell designer and supplier; cofunder

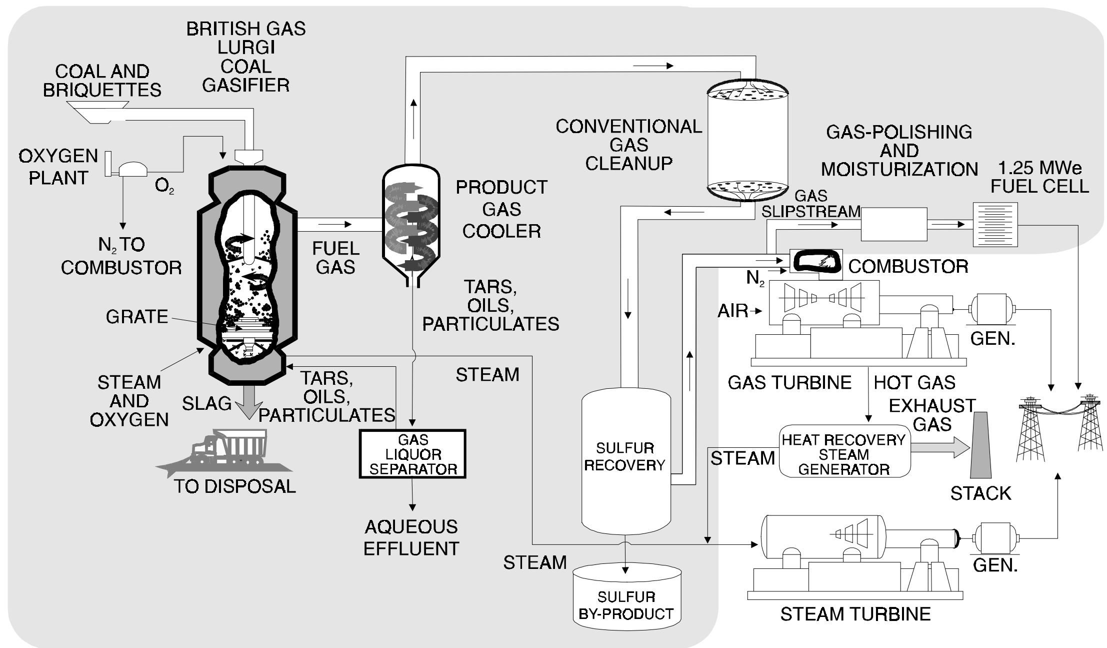
AMEREN Corporation—cofunder

Location
Carbondale, Jackson County, IL (Central Illinois Public Service Company's Grand Tower Station)

Technology
Integrated gasification combined-cycle (IGCC) using British Gas/Lurgi (BG/L) slagging fixed-bed gasification system coupled with Energy Research Corporation's molten carbonate fuel cell (MCFC)

Plant Capacity/Production
477-MWe (net) IGCC; 1.25-MWe MCFC

Coal
Illinois basin bituminous coal



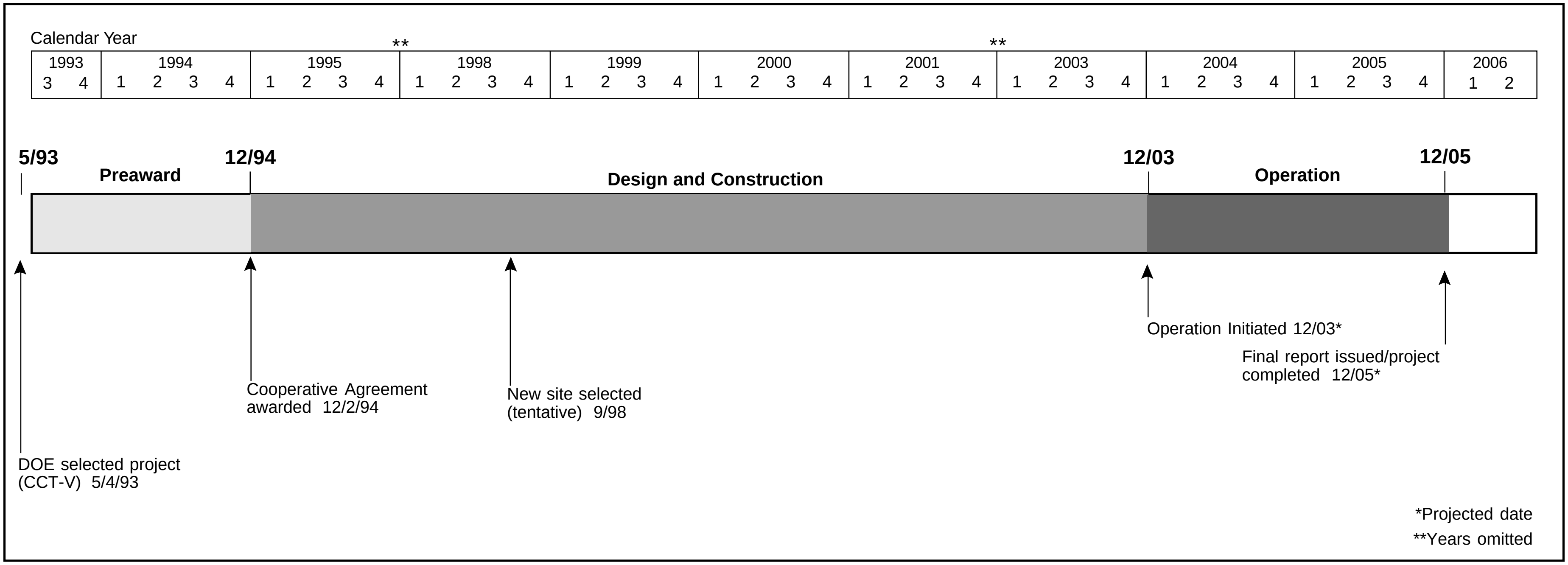
Project Funding

Total project cost	$841,096,189	100%
DOE	183,300,000	22
Participant	657,796,189	78

Project Objective
To demonstrate and assess the reliability, availability, and maintainability of a utility-scale IGCC system using high-sulfur bituminous coal in an oxygen-blown, fixed-bed, slagging gasifier and the operability of a molten carbonate fuel cell fueled by coal gas by an independent power producer under commercial terms and conditions.

Technology/Project Description
The BG/L gasifier is supplied with steam, oxygen, limestone flux, and coals having a high fines content. During gasification, the oxygen and steam react with the coal and limestone flux to produce a raw coal-derived fuel gas rich in hydrogen and carbon monoxide. Raw fuel gas exiting the gasifier is washed and cooled. Hydrogen sulfide and other sulfur compounds are removed. Elemental sulfur is reclaimed and disposed of as a by-product. Tars, oils, and dust are recycled to the gasifier. The resulting clean, medium-Btu fuel gas fires the gas turbine. A small portion of the clean fuel gas is used for the MCFC.

The MCFC is composed of a molten carbonate electrolyte sandwiched between porous anode and cathode plates. Fuel (desulfurized, heated medium-Btu fuel gas) and steam are fed continuously into the cathode. Electrical reactions produce direct electric current, which is converted to alternating power in an inverter.



Project Status/Accomplishments

The cooperative agreement was awarded December 2, 1994. Subsequent to award, a new site had to be found. The Central Illinois Public Service Company's Grand Tower Station was proposed by the Participant and approved by DOE on November 20, 1998.

Commercial Applications

The IGCC system being demonstrated in this project is suitable for both repowering applications and new power plants. The technology is expected to be adaptable to a wide variety of potential market applications because of several factors. First, the BG/L gasification technology has successfully used a wide variety of U.S. coals. Also, the highly modular approach to system design makes the BG/L-based IGCC and molten carbonate fuel cell competitive in a wide range of plant sizes. In addition, the high efficiency and excellent environmental performance of the system are competitive with or superior to other fossil-fuel-fired power generation technologies.

The heat rate of the IGCC demonstration facility is 8,560 Btu/kWh (40% efficiency) and the commercial embodiment of the system has a projected heat rate of 8,035 Btu/kWh (42.5% efficiency). The commercial version of the molten carbonate fuel cell fueled by a BG/L gasifier is anticipated to have a heat rate of 7,379 Btu/kWh (46.2% efficiency). These efficiencies represent greater than 20% reduction in emissions of CO_2 when compared to a conventional pulverized coal plant equipped with a scrubber. SO_2 emissions from the IGCC system are expected to be less than 0.1 lb/10^6 Btu (99% reduction); NO_x emissions, less than 0.15 lb/10^6 Btu (90% reduction).

Also, the slagging characteristic of the gasifier produces a nonleaching, glass-like slag that can be marketed as a usable by-product.

Piñon Pine IGCC Power Project

Participant
Sierra Pacific Power Company

Additional Team Members
Foster Wheeler USA Corporation—architect, engineer, and constructor
The M.W. Kellogg Company—technology supplier
Bechtel Corporation—startup engineer

Location
Reno, Storey County, NV (Sierra Pacific Power Company's Tracy Station)

Technology
Integrated gasification combined-cycle (IGCC) using the KRW air-blown pressurized fluidized-bed coal gasification system

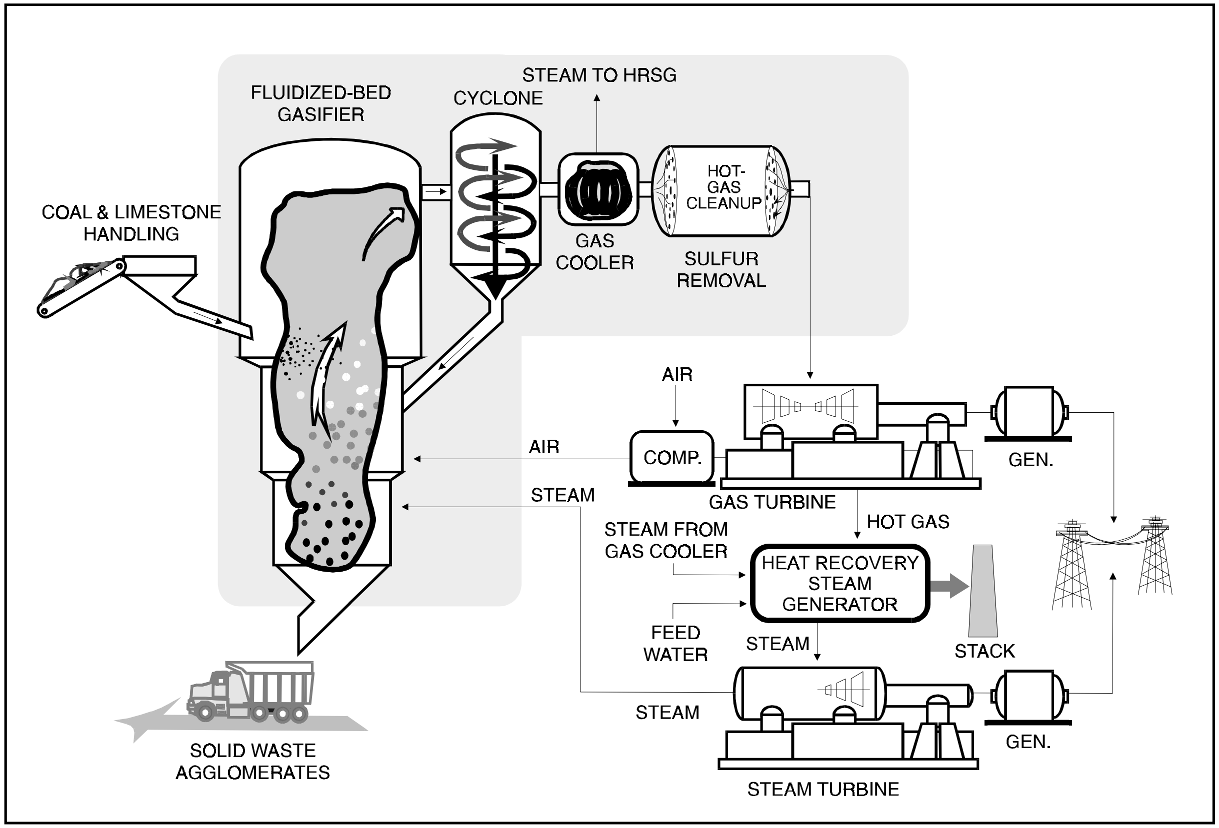
Plant Capacity/Production
107-MWe (gross), 99-MWe (net)

Coal
Southern Utah bituminous, 0.5–0.9% sulfur (design coal); eastern bituminous, 2–3% sulfur (planned test)

Project Funding

Total project cost	$335,913,000	100%
DOE	167,956,500	50
Participant	167,956,500	50

Project Objective
To demonstrate air-blown pressurized fluidized-bed IGCC technology incorporating hot gas cleanup; to evaluate a low-Btu gas combustion turbine; and to assess long-term reliability, availability, maintainability, and environmental performance at a scale sufficient to determine commercial potential.

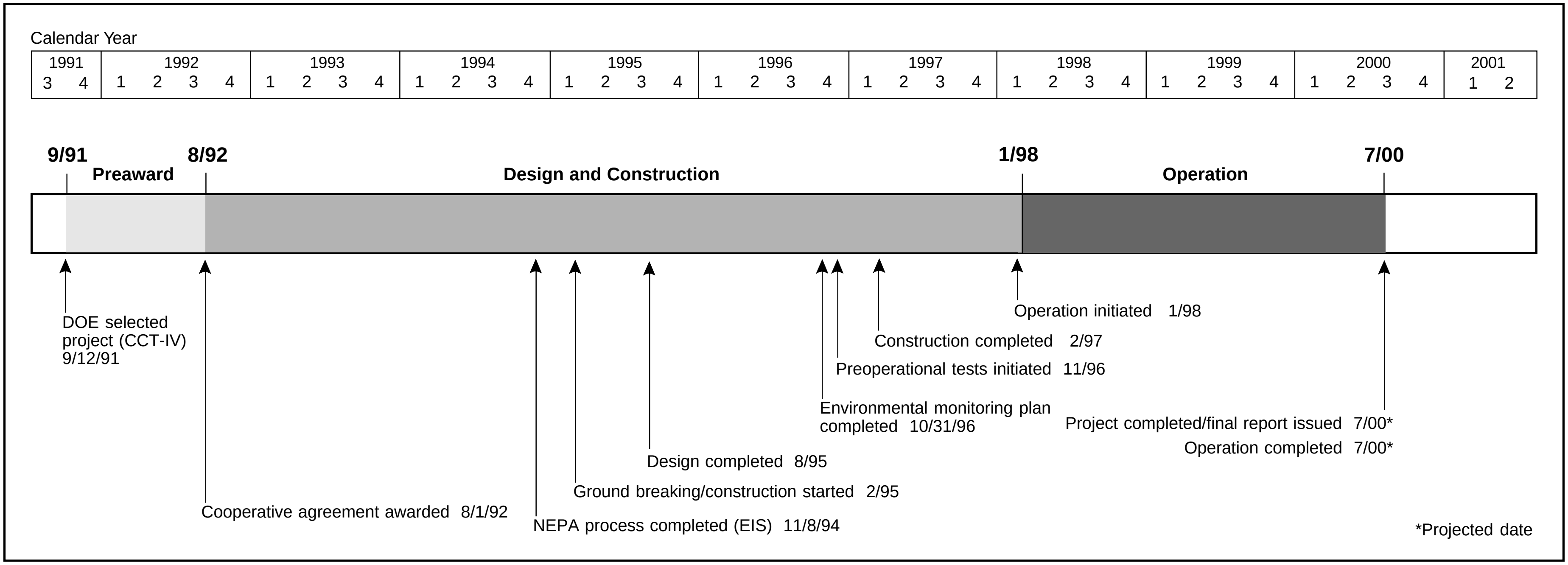


Technology/Project Description
Dried and crushed coal and limestone are introduced into an air-blown pressurized fluidized-bed gasifier. Crushed limestone is used to capture a portion of the sulfur and to inhibit conversion of fuel nitrogen to ammonia. The sulfur reacts with the limestone to form calcium sulfide which, after oxidation, exits as calcium sulfate along with the coal ash in the form of agglomerated particles suitable for landfill.

Low-Btu coal gas leaving the gasifier passes through cyclones, which return most of the entrained particulate matter to the gasifier. The gas, which leaves the gasifier at about 1,700 ºF, is cooled to about 1,100 ºF before entering the hot gas cleanup system. During cleanup, virtually all of the remaining particulates are removed by ceramic candle filters, and final traces of sulfur are removed by reaction with metal oxide sorbent in a transport reactor.

The cleaned gas then enters the GE Model MS6001FA combustion turbine, which is coupled to a generator designed to produce 61-MWe (gross). Exhaust gas is used to produce steam in a heat recovery steam generator. Superheated high-pressure steam drives a condensing steam turbine-generator designed to produce about 46-MWe (gross).

Due to the relatively low operating temperature of the gasifier and the injection of steam into the combustion fuel stream, the NO_x emissions are 0.069 lb/10^6 Btu (94% reduction). Due to the combination of in-bed sulfur capture and hot gas cleanup, SO_2 emissions are 0.069 lb/10^6 Btu (90% reduction).



In the demonstration project, 880 tons/day of coal are converted into 107 MWe (gross), or 99 MWe (net), for export to the grid. Southern Utah bituminous coal (0.5–0.9% sulfur) is the design coal; tests using midwestern or eastern high-sulfur bituminous coal (2–3% sulfur) also are planned. The integrated gasification system is located at Sierra Pacific Power Company's Tracy Station, near Reno, NV.

Project Status/Accomplishments

The system has initiated test-plan operations and continues to experience start-up problems. The station began operation on natural gas in November 1996. Pre-operational testing and shakedown of the coal gasification combined-cycle continued through 1997 with syngas produced in January 1998. The plant was dedicated in April 1998.

The GE Frame 6FA combustion turbine, the first of its kind in the world, has performed well since commencing operation in August 1996 on natural gas. Other portions of the plant have undergone design modification to improve performance, start-up logic for the gasifier has been revised, and an alternate sorbent for the transport desulfurizer was installed and successfully tested.

Short periods of steady-state gasifier operation on coal are routinely achieved. Sustained operation has been inhibited by mechanical and control problems in the hot gas filter system. Breakage of a significant number of candle filters was experienced due to failure of the fines combustor subsystem. Sierra Pacific also modified the bottom of the gasifier to correct a shift in the air/coal feed tube. While the gasifier was down for repair, Sierra Pacific repaired an area of the gasifier refractory that was eroded.

Commercial Applications

The Piñon Pine IGCC system concept is suitable for new power generation, repowering needs, and cogeneration applications. The net heat rate for a proposed greenfield plant using this technology is projected to be 7,800 Btu/kWh (43.7% efficiency), representing a 20% increase in thermal efficiency as compared to a conventional pulverized coal plant with a scrubber and a comparable reduction in CO_2 emissions. The compactness of an IGCC system reduces space requirements per unit of energy generated relative to other coal-based power generation systems. The advantages provided by phased modular construction reduce the financial risk associated with new capacity additions.

The KRW IGCC technology is capable of gasifying all types of coals, including high-sulfur, high-ash, low-rank, and high-swelling coals, as well as bio- or refuse-derived waste, with minimal environmental impact. There are no significant process waste streams that require remediation. The only solid waste from the plant is a mixture of ash and calcium sulfate, a nonhazardous waste.

Tampa Electric Integrated Gasification Combined-Cycle Project

Participant

Tampa Electric Company

Additional Team Members

Texaco Development Corporation—gasification technology supplier

General Electric Corporation—combined-cycle technology supplier

GE Environmental Services, Inc.—hot-gas cleanup technology supplier

TECO Power Services Corporation—project manager and marketer

Bechtel Power Corporation—architect and engineer

Location

Mulberry, Polk County, FL (Tampa Electric Company's Polk Power Station, Unit No. 1)

Technology

Integrated gasification combined-cycle (IGCC) system using Texaco's pressurized oxygen-blown entrained-flow gasifier technology and incorporating both conventional low-temperature acid-gas removal and hot-gas moving-bed desulfurization

Plant Capacity/Production

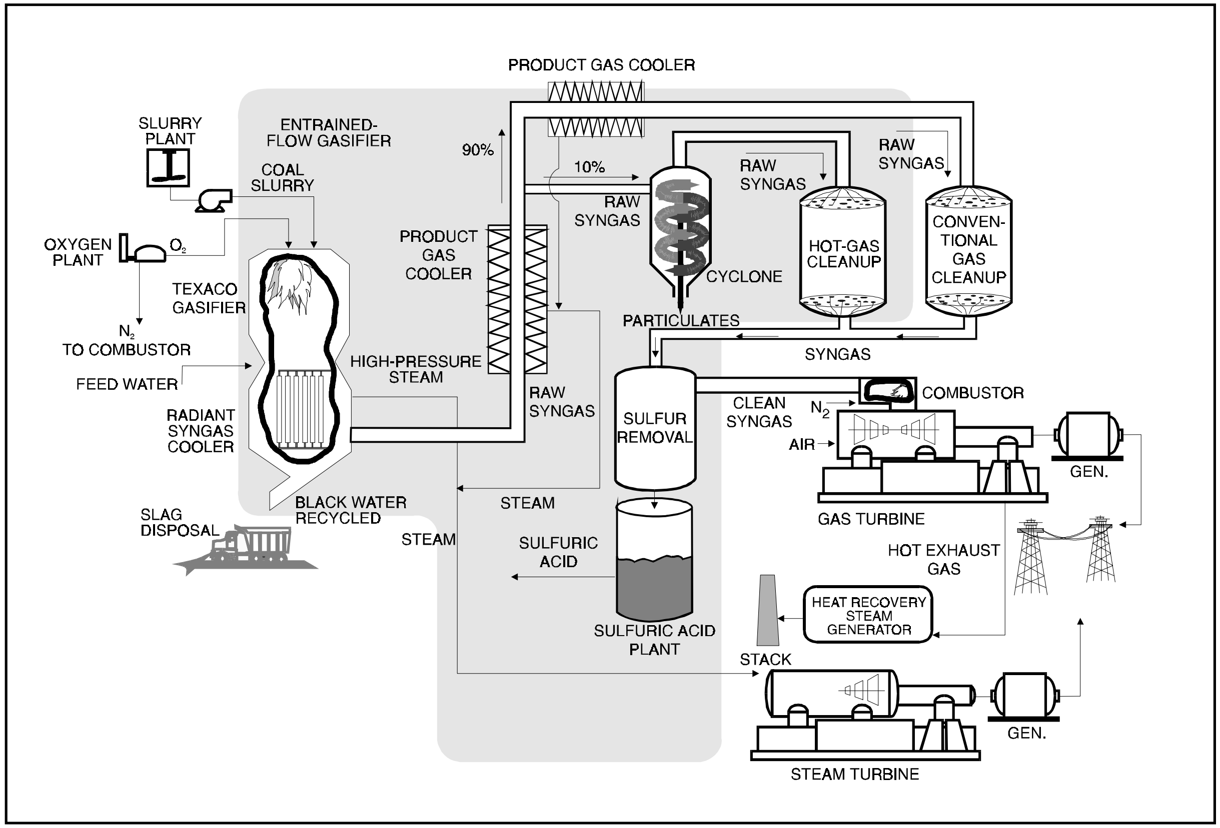
250-MWe (net)

Coal

Illinois #6, Pittsburgh #8, Kentucky #11, 2.5–3.5% sulfur

Project Funding

Total project cost	$303,288,446	100%
DOE	150,894,223	49
Participant	152,394,223	51



Project Objective

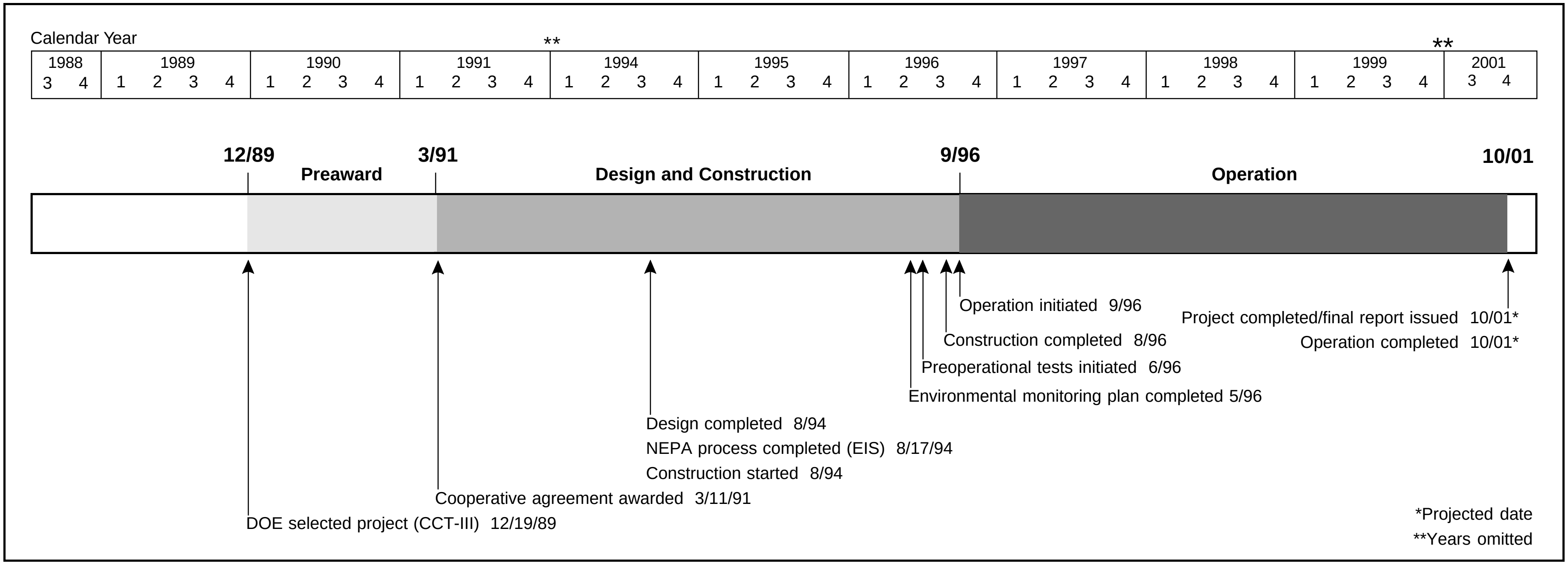
To demonstrate IGCC technology in a greenfield, commercial, electric utility application at the 250-MWe size with a Texaco gasifier; to demonstrate the integrated performance of a metal oxide hot-gas cleanup system, conventional cold-gas cleanup, and an advanced gas turbine with nitrogen injection (from the air separation plant) for power augmentation and NO_x control.

Technology/Project Description

Texaco's pressurized, oxygen-blown, entrained-flow gasifier is used to produce a medium-Btu fuel gas. Coal/water slurry and oxygen are reacted at high temperature and pressure to produce a high-temperature syngas. The syngas from the gasifier moves to a high-temperature heat-recovery unit, which cools the gases. Molten coal-ash flows out of the bottom of the vessel and into a water-filled quench tank where it is forms a solid slag.

The cooled gases flow to a particulate-removal section before entering gas-cleanup trains. A portion of the syngas (10%) is passed through a moving bed of metal oxide absorbent to remove sulfur. The remaining syngas is further cooled through a series of convective heat exchangers before entering a conventional gas-cleanup train where sulfur is removed by an acid-gas removal system. Combined, these cleanup systems are expected to maintain sulfur levels below 0.21 lb/10^6 Btu (96% capture). The cleaned gases are then routed to a combined-cycle system for power generation. Sulfuric acid and slag are salable by-products.

A GE MS 7001F gas turbine generates about 192 MWe (gross). Thermal-NO_x is controlled to below



0.27 lb/10^6 Btu by injecting nitrogen as a dilutent in the turbine's combustion section. A heat-recovery steam-generator produces an additional 121-MWe (gross). Polk's IGCC heat rate for this demonstration is expected to be approximately 8,600 Btu/kWh (40% efficient). The demonstration project involves only the first 250-MWe (net) of the planned 1,150-MWe Polk Power Station. Illinois #6, and Pittsburgh #8, and Kentucky #11 bituminous coals (2.5–3.5% sulfur) are being used.

Project Status/Accomplishments

The plant began commercial operation in September 1996 and continues to successfully accumulate run time. Gasifier operation had exceeded 10,000 hours by October 1998. The gasifier on-stream factor steadily increases over time, reaching 70% for the past 12 months. Combined-cycle availability has remained above 90% since the second quarter of 1997. Improved gasifier availability was largely due to removal of the raw gas/clean gas heat exchanger, a source of particulate contamination, and installation of a larger filter to prevent leakage of particulate matter to the turbine. Also contributing to improved availability are new operating procedures to deal with radiant syngas cooler dome seal leaks and hot restarts of the gasifier.

Recent tests included evaluation of various coal types on system performance. Kentucky #11, Illinois #6, and three Pittsburgh #8 coals were tested for their: (1) ability to be processed into a high concentration slurry, (2) carbon conversion efficiency, (3) aggressiveness of the slag in regard to refractory wear, and (4) tendency toward fouling of the syngas coolers. Kentucky #11 coal proved to have the best overall characteristics and supplanted Pittsburgh #8 as the base coal. Illinois #6 placed second and prompted further testing because of some promising aspects of its performance.

Commercial Applications

This demonstration project is scaling up the technology from Cool Water demonstration unit (100-MWe) tested without full system integration. The Texaco-based IGCC is suitable for new electric power generation, repowering needs, and cogeneration applications. Commercial IGCCs should achieve better than 98% SO_2 capture with a NO_x emissions reduction of 90% relative to a conventional pulverized coal-fired plant.

Texaco and ASEA Brown Boveri have signed an agreement forming an alliance to market IGCC technology in Europe.

The project was presented the 1997 Powerplant Award by *Power* magazine. In 1996 the project received the Association of Builders and Contractors Award for construction quality. Several awards were presented for using an innovative siting process: 1993 Ecological Society of America Corporate Award, 1993 Timer Powers

Wabash River Coal Gasification Repowering Project

Participant
Wabash River Coal Gasification Repowering Project Joint Venture (a joint venture of Dynegy and PSI Energy, Inc.)

Additional Team Members
PSI Energy, Inc.—host
Dynegy (formerly Destec Energy, Inc.)—engineer, gas plant operator, and technology supplier

Location
West Terre Haute, Vigo County, IN (PSI Energy's Wabash River Generating Station, Unit No. 1)

Technology
Integrated gasification combined-cycle (IGCC) using Destec's two-stage pressurized oxygen-blown entrained-flow gasification system

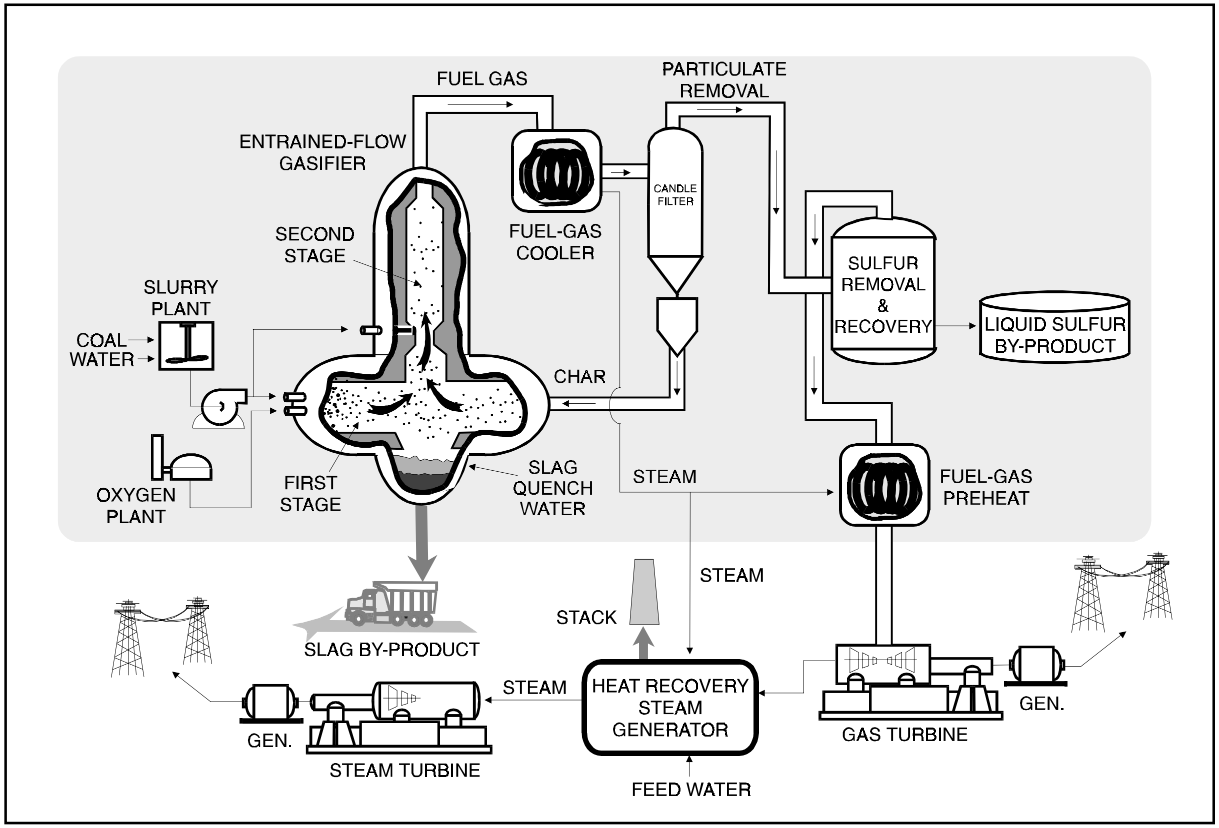
Plant Capacity/Production
296-MWe (gross), 262-MWe (net)

Coal
Illinois Basin bituminous

Project Funding

Total project cost	$438,200,000	100%
DOE	219,100,000	50
Participant	219,100,000	50

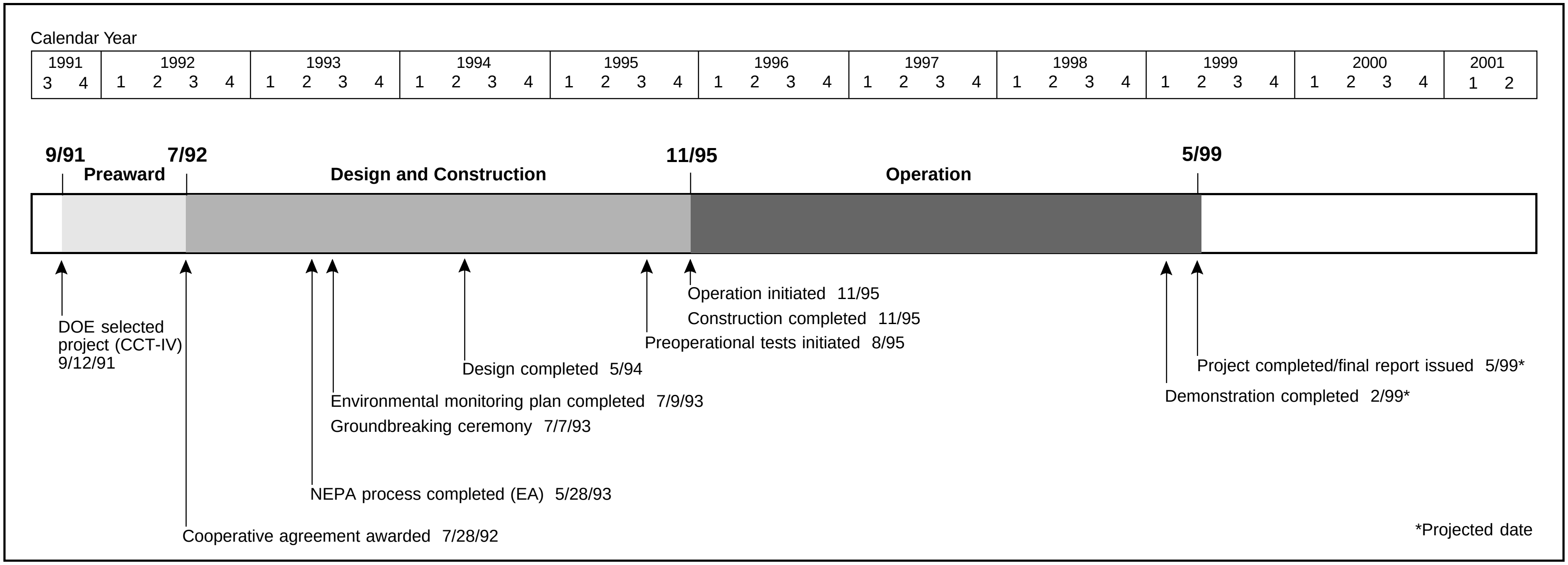
Project Objective
To demonstrate utility repowering with a two-stage pressurized oxygen-blown entrained-flow IGCC system, including advancements in the technology relevant to the use of high-sulfur bituminous coal and to assess long-term reliability, availability, and maintainability of the system at a fully commercial scale.



Technology/Project Description
Coal is ground in a rod mill slurried with water, and gasified in a pressurized, two-stage (slagging first stage and non-slagging entrained-flow second stage), oxygen-blown, gasifier. The product gas is cooled through heat exchangers and passed through a conventional cold gas cleanup system which removes particulates, ammonia, and sulfur. The clean, medium-Btu gas is then reheated and burned in an advanced 192-MWe (gross) GE 7FA (MS 7001) gas turbine. Hot exhaust from the gas turbine is passed through a heat recovery steam generator to produce high-pressure steam. High-pressure steam is also produced from the gasification plant and superheated in the heat recovery steam generator. The combined high-pressure steam flow is supplied to an existing, refurbished 104-MWe (gross) steam turbine for a total output of 296 MWe (gross).

The process has the following subsystems: a coal-grinding and slurry system, an entrained-flow coal gasifier, a syngas heat recovery system, a cold gas cleanup system that produces a marketable sulfur by-product, a combustion turbine capable of using coal-derived fuel gas, a heat recovery steam generator, and a repowered steam turbine.

One of six units at Wabash River Generating Station was repowered. The demonstration unit generates 262-MWe (net) using 2,544 tons/day of high-sulfur (2.3–5.9% sulfur) Illinois Basin bituminous coal. The anticipated heat rate for the repowered unit is approximately 9,000 Btu/kWh (38% efficiency). Using high-sulfur bituminous coal, SO_2 emissions are expected to be



less than 0.1 lb/10^6 Btu (98% reduction). NO_x emissions are expected to be less than 0.1 lb/10^6 Btu (90% reduction). The project represents the world's largest single-train IGCC plant currently in operation.

Project Status/Accomplishments

The project began operations in November 1995 and continues in its third year of commercial service. CINergy, PSI's post-merger parent company, preferentially dispatches the unit second behind its hydro facilities on the basis of environmental emissions and efficiency, with a demonstrated heat rate of better than 9,000 Btu/kWh (HHV). Late 1998 operating statistics showed an annual availability of 77.2%. Since initiating operation in 1995, the unit has achieved monthly production levels of one trillion Btus on four occasions. Refinements to the design are continuing, including replacement of ceramic candle particulate filters with a metallic filter (operating temperature 800 ºF) and installation of a chloride scrubber and new COS hydrolysis catalyst for SO_2 control.

Both the gasifier and combined-cycle plants have demonstrated the ability to run at capacity and within environmental compliance while using locally mined, high sulfur coal. Early identification of availability limiting process problems within the gasification plant led to aggressive implementation of improvements which have nearly tripled production since operations began.

Commercial Applications

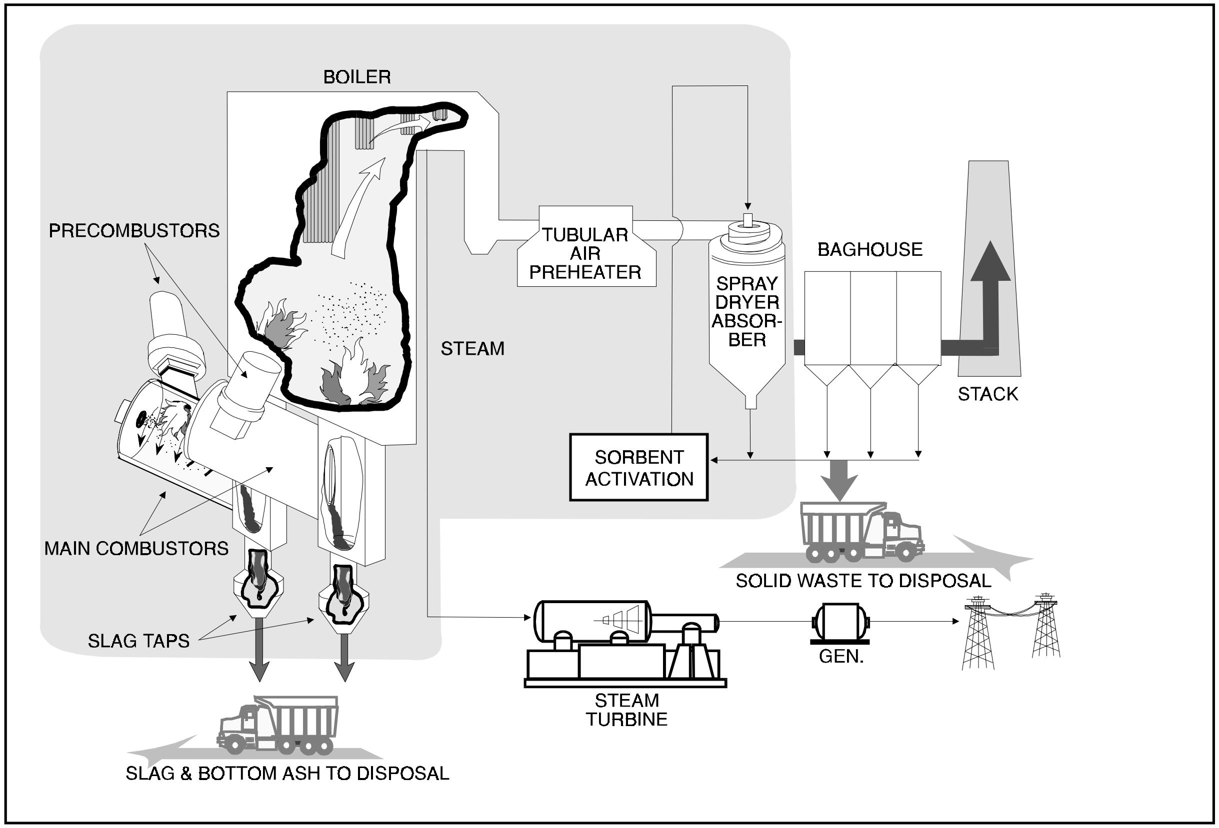
Throughout the United States, particularly in the Midwest and East, there are more than 95,000-MWe of existing coal-fired utility boilers over 30 years old. Many of these aging plants are without air pollution controls and are candidates for repowering with IGCC technology. Repowering these plants with IGCC systems will improve plant efficiencies and reduce SO_2, NO_x, and CO_2 emissions. The modularity of the gasifier technology will permit a range of units to be considered for repowering, and the relatively short construction schedule for the technology will allow utilities greater flexibility in designing strategies to meet load requirements. Also, the high degree of fuel flexibility inherent in the gasifier design will provide utilities with more choice in selecting fuel supplies to meet increasingly stringent air quality regulations.

Given the advantages of modularity, rapid and staged on-line generation capability, high efficiency, fuel flexibility, environmental controllability, and reduced land and natural resource needs, the IGCC system is also a strong contender for new electric power generating facilities. Commercial offerings of the technology will be based on a 300-MWe train, which is ideally suited to utility-scale power generation applications. The system heat rate for a new power plant based on this technology is expected to realize at least a 20% improvement in efficiency compared to a conventional pulverized-coal-fired plant with flue gas desulfurization. The improved system efficiency also results in a similar decrease in CO_2 emissions.

Destec Energy and CINergy Corp./PSI Energy received the 1996 Powerplant Award from *Power* magazine. Sargent & Lundy, engineer for the combined-cycle facility, won the American Consulting Engineers Council's 1996 Engineering Excellence Award.

Advanced Electric Power Generation
Advanced Combustion/Heat Engines

Healy Clean Coal Project



Participant
Alaska Industrial Development and Export Authority

Additional Team Members
Golden Valley Electric Association—operator
Stone and Webster Engineering Corp.—engineer
TRW Inc., Space & Technology Division—combustor technology supplier
The Babcock & Wilcox Company (which has acquired assets of Joy Environmental Technologies, Inc.)—spray-dryer absorber technology supplier
Usibelli Coal Mine, Inc.—coal supplier

Location
Healy, Denali Borough, AK (adjacent to Healy Unit No. 1)

Technology
TRW's advanced entrained (slagging) combustor
Babcock & Wilcox's spray-dryer absorber with sorbent recycle

Plant Capacity/Production
50-MWe (nominal)

Coal
Usibelli subbituminous 35% run-of-mine (0.2% sulfur) and 65% waste coal (design)

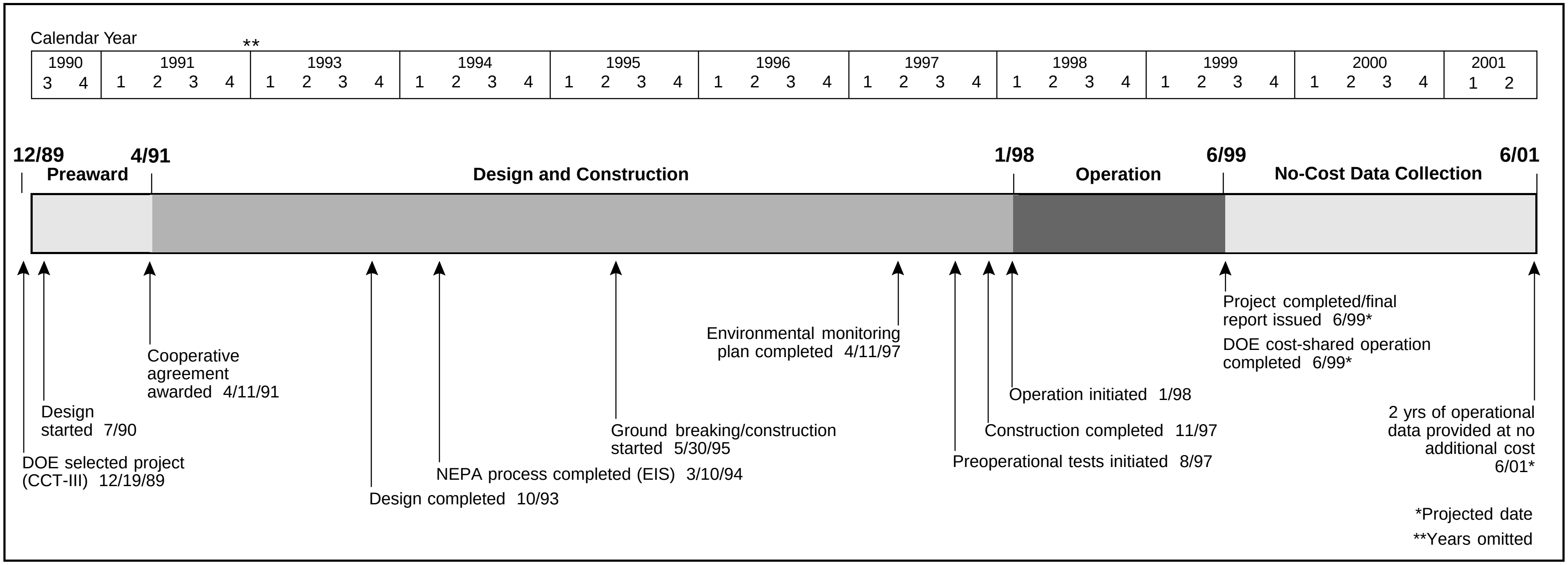
Project Funding

Total project cost	$242,058,000	100%
DOE	117,327,000	48
Participant	124,731,000	52

Project Objective
To demonstrate an innovative new power plant design featuring integration of an advanced combustor and heat recovery system coupled with both high- and low-temperature emissions control processes.

Technology/Project Description
The project involves two unique slagging combustors generating a nominal 50-MWe. Emissions of SO_2 and NO_x are controlled using TRW's slagging combustion systems with staged fuel and air, a boiler that controls fuel- and thermal-NO_x related conditions, and limestone injection. Additional SO_2 is removed using Babcock & Wilcox's activated recycle spray-dryer absorber system. Performance goals are NO_x emissions of less than 0.2 lb/10^6 Btu, particulate emissions of 0.015 lb/10^6 Btu, and SO_2 removal greater than 90%. The design fuel blend performance testing of coal consists of 35% run-of-mine and 65% waste coal.

A coal-fired precombustor increases the air inlet temperature for optimum slagging performance. The TRW slagging combustors are side mounted, injecting the combustion products vertically into the boiler. The main slagging combustor consists of a water-cooled cylinder that slopes toward a slag opening. The precombustor burns 25–40% of the total coal input. The remaining coal is injected axially into the combustor, rapidly entrained by the swirling precombustor gases and additional air flow, and burned under substoichio-metric (fuel-rich) conditions for NO_x control. The ash forms molten slag, which accumulates on the water-cooled walls and is driven by aerodynamic and gravitational forces through a slot into the slag recovery section. About 70–80% of the coal's ash is removed as molten slag. The hot gas is then ducted to the furnace where, to ensure complete combustion,



additional air is supplied from the tertiary air windbox to NO_x ports and to final overfire air ports.

Pulverized limestone ($CaCO_3$) for SO_2 control is fed into the combustor where it is flash calcined (converting $CaCO_3$ to CaO). The mixture of this lime (CaO) and ash not slagged, called flash-calcined material, is removed in the fabric filter (baghouse) system. Most of the flash-calcined material is used to form a 45% flash-calcined-material solids slurry. SO_2 in the flue gas reacts with the slurry droplets as water is simultaneously evaporated. SO_2 is further removed from the flue gas by reacting with the dry flash-calcined material on the baghouse filter bags.

The project site is adjacent to the existing Healy Unit No. 1 near Healy, AK, and to the Usibelli coal mine. Power will go to the Golden Valley Electric Association (GVEA). The plant will use 900 tons/day of subbituminous coal and waste coal. The project will collect performance data for 3½ years, with 2 years of data being provided at no cost to DOE. A hazardous air pollutant monitoring program will also be implemented.

To address concerns about potential impact to the nearby Denali National Park and Preserve, DOE, the National Park Service, GVEA, and the project participant entered into an agreement to reduce the emissions from Unit No. 1 so that the combined emissions from the two units will be only slightly greater than those currently emitted from Unit No. 1 alone. Total site emissions will be further reduced to current levels if necessary to protect the park.

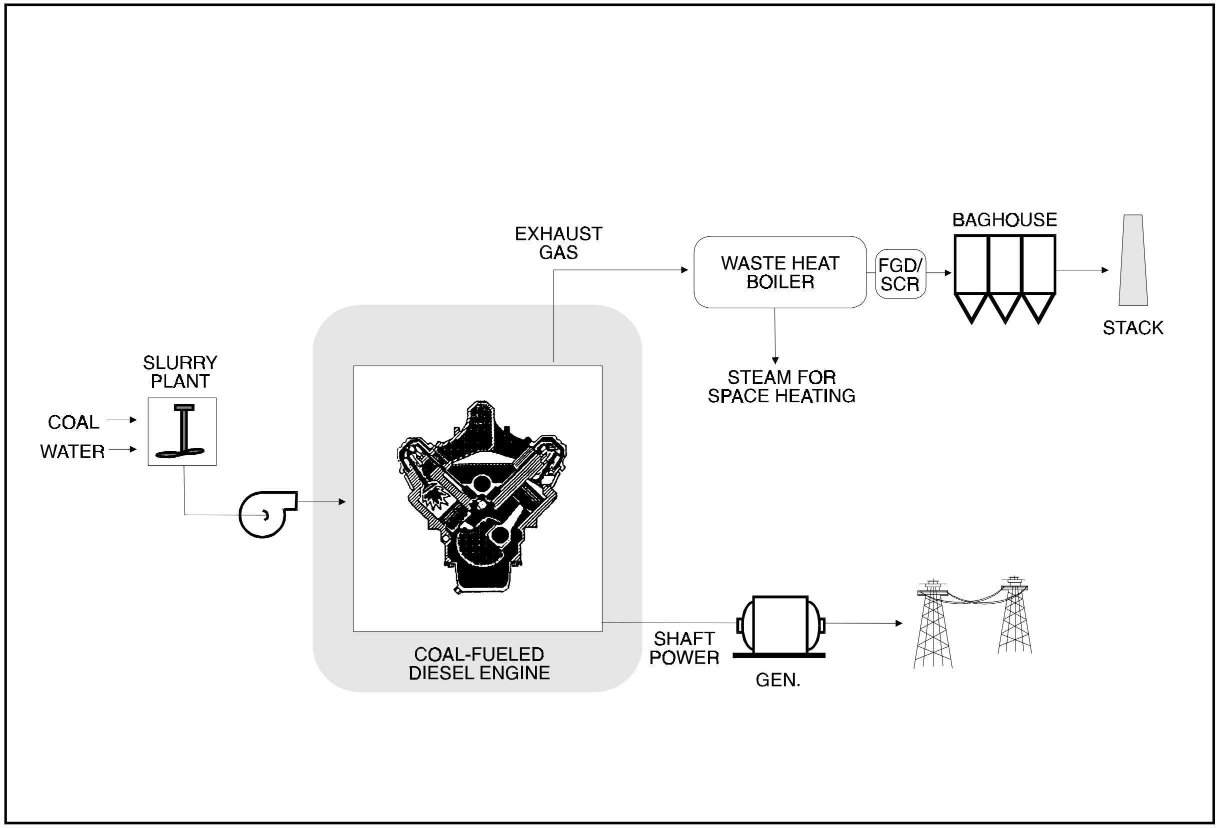
Project Status/Accomplishments

Start-up of the entrained slagging combustion system began in January 1998. During a record-setting 18-day period of continuous operation, initial NO_x and SO_2 environmental compliance testing was completed. The preliminary results showed that NO_x emissions of 0.25 lb/10^6 Btu and SO_2 emissions of 0.08 lb/10^6 Btu were achieved. The permit requires emissions to be less than 0.35 lb/10^6 Btu for NO_x and less than 0.10 lb/10^6 Btu for SO_2. The stringent SO_2 emission level required by the permit is significantly lower than the 1.2 lb/10^6 Btu NSPS limit. The environmental compliance testing was witnessed by the U.S. EPA, Region X and the Alaska Department of Environmental Conservation. The plant was experiencing precombustor plugging when the coal feed is changed to a 50/50 blend of run-of-mine and waste coal. The main problem remaining is solid particle erosion of the mill exhauster fans.

Commercial Applications

This technology has a wide range of applications. It is appropriate for any size utility or industrial boiler in new and retrofit uses. It can be used in coal-fired boilers as well as in oil- and gas-fired boilers because of its high ash-removal capability. However, cyclone boilers may be the most amenable type to retrofit with the slagging combustor because of the limited supply of high-Btu, low-sulfur, low-ash-fusion-temperature coal that cyclone boilers require. The commercial availability of cost-effective and reliable systems for SO_2, NO_x, and particulate control is important to potential users planning new

Clean Coal Diesel Demonstration Project



Participant
Arthur D. Little, Inc.

Additional Team Members
University of Alaska at Fairbanks—host and cofunder
Alaskan Science & Technology Foundation—cofunder
Coltec Industries Inc.—diesel engine technology vendor
Energy and Environmental Research Center, University of North Dakota—fuel preparation technology vendor
R.W. Beck, Inc.—architect/engineer, designer, constructor
Usibelli Coal Mine, Inc.—coal supplier

Location
Fairbanks, AK (University of Alaska facility)

Technology
Coltec's coal-fueled diesel engine

Plant Capacity/Production
6.4-MWe (net)

Coal
Usibelli Alaskan subbituminous

Project Funding

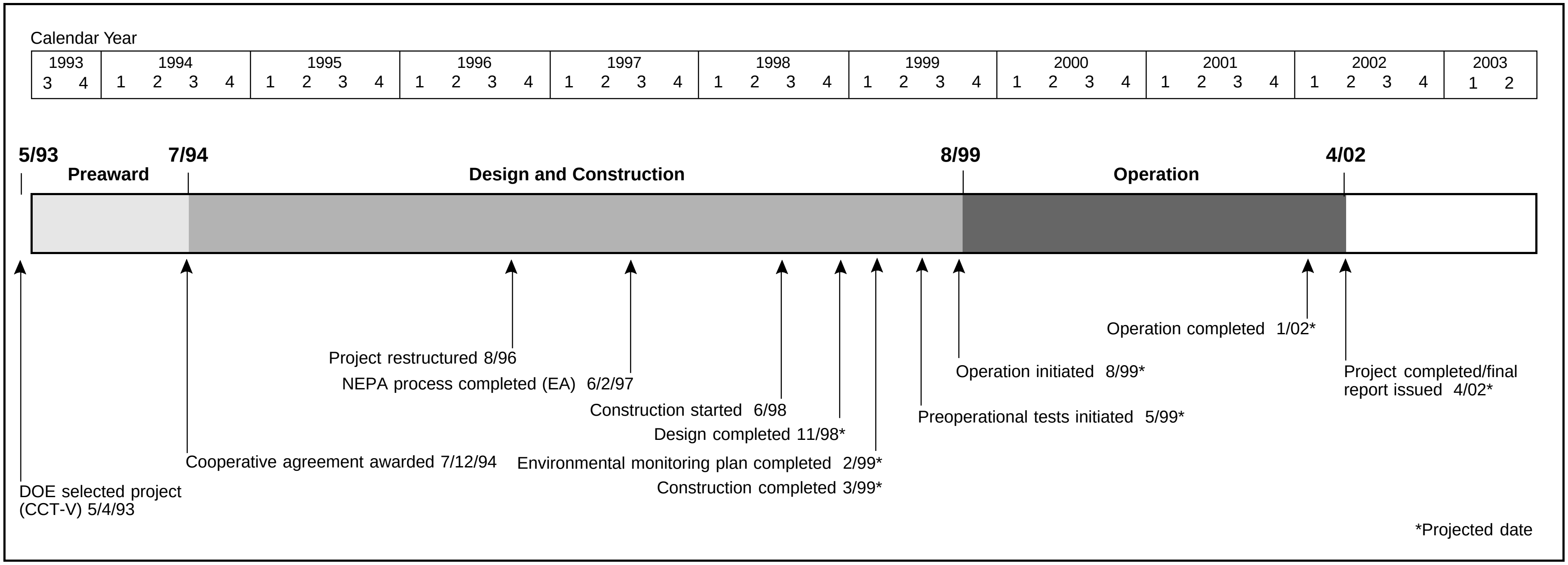
Total project cost	$47,636,000	100%
DOE	23,818,000	50
Participant	23,818,000	50

Project Objective
To prove the design, operability, and durability of the coal diesel engine during 6,000 hours of operation; verify the design and operation of an advanced drying/slurrying process for subbituminous Alaskan coals; and test the coal slurry in the diesel and a retrofitted oil-fired boiler.

Technology/Project Description
The project is based on the demonstration of an 18-cylinder, heavy duty engine (6.4-MWe) modified to operate on Alaskan subbituminous coal. The clean coal diesel technology, which uses a low-rank coal-water-fuel (LRCWF) slurry, is expected to have very low NO_x and SO_2 emission levels (50–70% below current New Source Performance Standards). In addition, the demonstration plant is expected to achieve 41% efficiency, while future plant designs are expected to reach 48% efficiency. This will result in a 25% reduction in CO_2 compared to conventional coal-fired plants.

The LRCWF is prepared using an advanced coal drying process that allows dried coal to be slurried in water. The University of Alaska will assemble and operate a 5-ton/hr LRCWF processing plant that will utilize local coal brought by truck from Usibelli's mine in Healy, AK. In addition to its use in the coal-fueled diesel engine, the LRCWF is expected to be an alternative to fuel oil in conventional oil-fired industrial boilers.

Project Status/Accomplishments
The project has passed several milestones. A 60% design review was conducted in March 1998 at the University of Alaska, Fairbanks (UAF). Representatives from Coltec, A.D. Little, UAF, DOE, and GHEMM (construction contractor) were in attendance. The new design eliminates the sorbent injection system, since Usibelli was able to locate a very clean coal seam with less than 0.2% sulfur in the ash. The sorbent injection system originally proposed for the coal diesel was designed for use with bituminous coals with greater than 2.0% sulfur



levels. Coltec worked with the diesel engine manufacturer to design new injectors with sapphire orifices sized for the volume of LRCWF required to operate the engine at full load. Earlier designs were based on higher energy density bituminous coals.

Delivery of the 18-cylinder diesel engine has moved to January 1999. Construction activities started at the Fairbanks site on June 15, 1998 and construction is over 60% complete.

Samples of the Usibelli coal were sent to CQ Inc., for washability tests; ADL for wear tests; and to EERC for preliminary hot water drying tests. Several plant design changes were made in order to keep the project within budget. Notably, only a small oil-fired boiler will be converted for coal slurry tests instead of a utility-scale boiler, and several of the slurry holding tanks will be located closer to the diesel engine to reduce underground piping.

Commercial Applications

The coal-fueled diesel engine is particularly suited for nonutility new capacity, small utility repowering, and exports to developing countries. The net effective heat rate for the mature diesel system is expected to be 6,830 Btu/kWh (48%), which makes it very competitive with similarly sized coal- and fuel oil-fired installations. Environmental emissions from commercial diesel systems should be reduced to levels between 50% and 70% below NSPS. The estimated installation cost of a mature commercial unit is approximately $1,300/kW.

The U.S. diesel market is projected to exceed 60,000-MWe (over 7,000 engines) through 2020. The worldwide market is 70 times the U.S. market. The technology is particularly applicable to dispersed power generation in the 5–20-MWe range, using indigenous coal in developing countries.

Coal Processing for Clean Fuels

Commercial-Scale Demonstration of the Liquid-Phase Methanol (LPMEOH™) Process

Participant

Air Products Liquid Phase Conversion Company, L.P. (a limited partnership between Air Products and Chemicals, Inc., the general partner, and Eastman Chemical Company)

Additional Team Members

Air Products and Chemicals, Inc.—technology supplier and cofunder

Eastman Chemical Company—host, operator, synthesis gas and services provider

ARCADIS Geraghty & Miller—fuel methanol tester and cofunder

Electric Power Research Institute—utility advisor

Location

Kingsport, Sullivan County, TN (Eastman Chemical Company's Integrated Coal Gasification Facility)

Technology

Air Products and Chemicals' liquid phase methanol (LPMEOH™) process

Plant Capacity/Production

80,000 gallons/day of methanol (nominal)

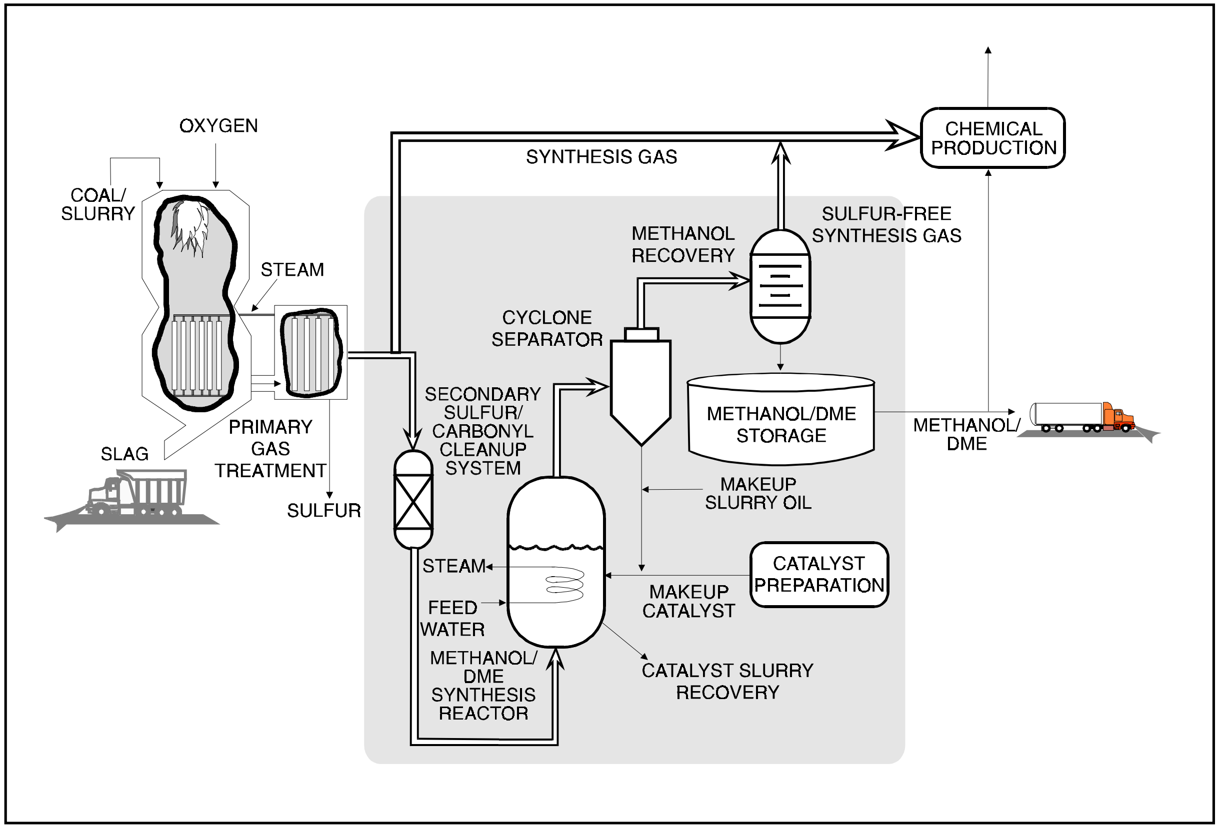
Coal

Eastern high-sulfur bituminous, 3–5% sulfur

Project Funding

Total project cost	$213,700,000	100%
DOE	92,708,370	43
Participant	120,991,630	57

LPMEOH™ is a trademark of Air Products and Chemicals, Inc.



Project Objective

To demonstrate on a commercial scale the production of methanol from coal-derived synthesis gas using the LPMEOH™ process; to determine the suitability of methanol produced during this demonstration for use as a chemical feedstock or as a low-SO_x, low-NO_x alternative fuel in stationary and transportation applications; and to demonstrate, if practical, the production of dimethyl ether (DME) as a mixed coproduct with methanol.

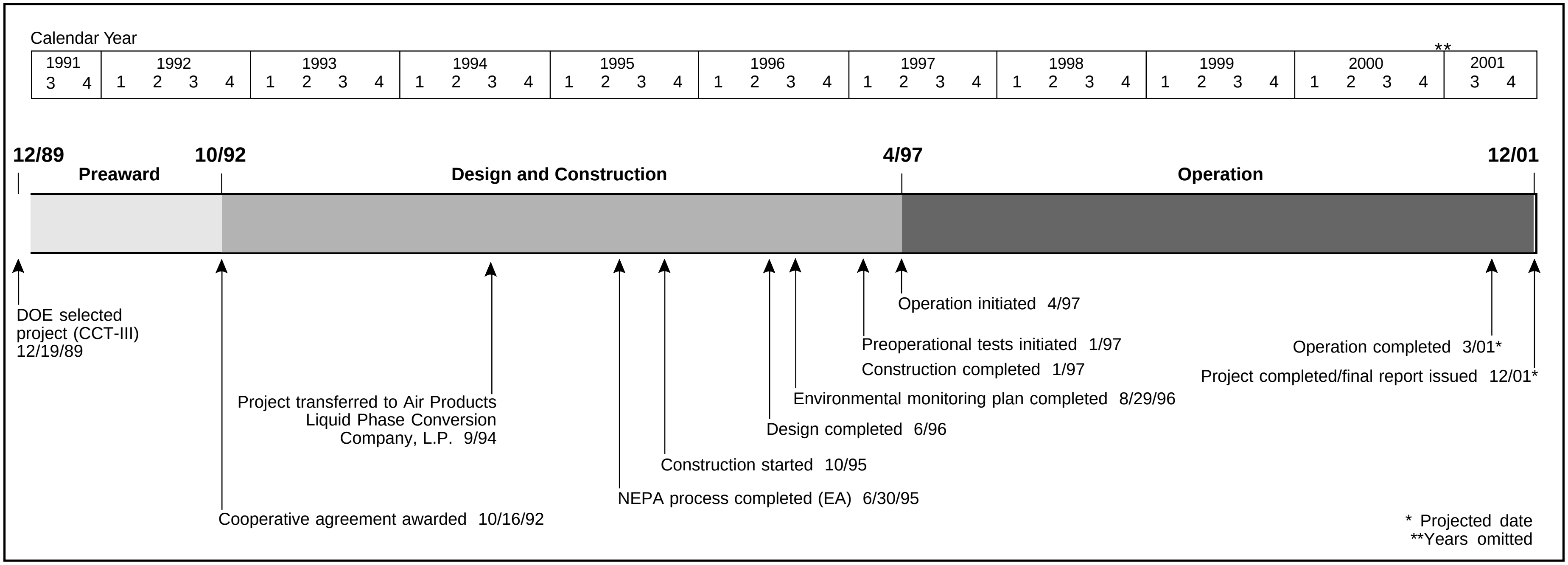
Technology/Project Description

This project is demonstrating, at commercial scale, the LPMEOH™ process to produce methanol from coal-derived synthesis gas. The combined reactor and heat removal system is different from other commercial methanol processes. The liquid phase not only suspends the catalyst but functions as an efficient means to remove the heat of reaction away from the catalyst surface. This feature permits the direct use of synthesis gas streams as feed to the reactor without the need for phase-shift conversion.

Methanol fuel testing will be conducted in off-site stationary and mobile applications, such as fuel cells, buses, and distributed electric power generation. Design verification testing for the production of DME as a mixed coproduct with methanol for use as a storable fuel is planned, and a decision on whether or not to demonstrate will be made. Eastern high-sulfur bituminous coal (Mason seam) containing 3% sulfur (5% maximum) and 10% ash will be used.

Project Status/Accomplishments

Construction was completed in January of 1997. Fol-



lowing commissioning and shakedown activities, the first production of methanol from the 80,000 gal/day unit occurred on April 2, 1997. The first stable operation of the process demonstration unit at nameplate capacity occurred on April 6, 1998. A stable test period at over 92,000 gal/day revealed no system limitations. The startup also proceeded without injury or environmental incidents.

During calendar year 1997, availability of the process demonstration unit exceeded 92%. The hydrogen to carbon monoxide (H_2/CO) ratio in the reactor feed stream was varied from 0.4 to 5.6 with no negative effects on catalyst performance. The operation of the demonstration unit confirmed the engineering methods used in the design of the LPMEOH™ Reactor, and several parameters (such as the overall heat transfer coefficient of the internal heat exchanger) were demonstrated at greater than 115% of design levels.

Operation during 1998 has resulted in significant accomplishments. The design catalyst loading in the LPMEOH™ Reactor has been exceeded without indications of mass transfer limitations. Since being restarted with fresh catalyst in December of 1997, the demonstration facility has operated at greater than 99% availability, and 67 days of what would be a 94-day period of continuous operation was in progress as of September 30, 1998. Catalyst life has met or exceeded the design target for operation in the environment of trace poisons present in coal-derived synthesis gas. Process variable studies to maximize the reactor volumetric productivity and determine the long-term catalyst performance are on-going. Since startup, the demonstration facility has produced over 25 million gallons of methanol, all of which has been accepted by Eastman Chemical Company for use in downstream chemical processes.

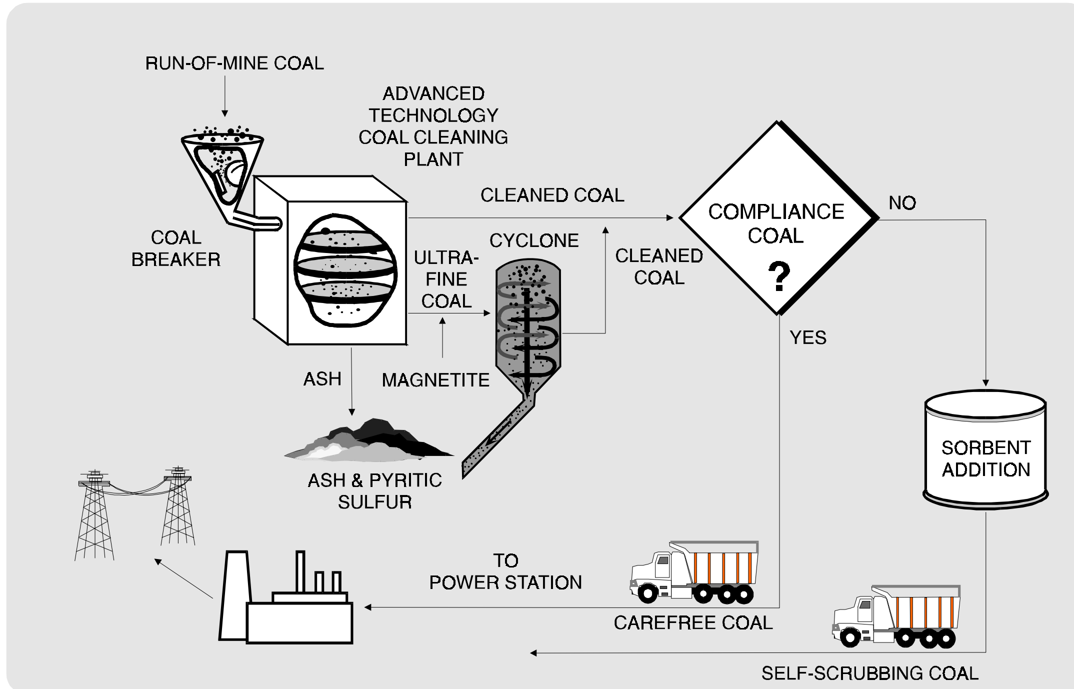
Commercial Applications

The LPMEOH™ process has been developed to enhance integrated gasification combined-cycle (IGCC) power generation by producing a clean burning, storable liquid fuel—methanol—from the clean coal-derived gas. Methanol also has a broad range of commercial applications, can be substituted for conventional fuels in stationary and mobile combustion applications, is an excellent fuel for utility peaking units, contains no sulfur, and has exceptionally low-NO_x characteristics when burned. Methanol can be produced from coal as a coproduct in an IGCC facility.

DME has several commercial uses. In a storable blend with methanol, the mixture can be used as peaking fuel in IGCC electric power generating facilities. Blends of methanol and DME can also be used as a chemical feedstock for the synthesis of chemicals or new, oxygenate fuel additives. Pure DME is an environmentally friendly aerosol for personal products.

Typical commercial-scale LPMEOH™ units are expected to range in size from 50,000–300,000 gal/day of methanol produced when associated with commercial IGCC power generation trains of 200–500 MWe. Air

Self-Scrubbing Coal™: An Integrated Approach to Clean Air



Participant
Custom Coals International

Additional Team Members
Pennsylvania Power & Light Company—host
Richmond Power & Light—host
Centerior Service Company—host

Locations
Central City, Somerset County, PA (advanced coal-cleaning plant)
Lower Mt. Bethel Township, Northampton County, PA (combustion tests at Pennsylvania Power & Light's Martin's Creek Power Station, Unit No. 2)
Richmond, Wayne County, IN (combustion tests at Richmond Power & Light's Whitewater Valley Generating Station, Unit No. 2)
Ashtabula, Trumbull County, OH (combustion tests at Centerior Energy's Ashtabula C)

Technology
Coal preparation using Custom Coals' advanced physical coal-cleaning and fine magnetite separation technology plus sorbent addition technology

Plant Capacity/Production
500 tons/hr

Coals
Medium and high-sulfur bituminous

Project Funding

Total project cost	$87,386,102	100%
DOE	37,994,437	43
Participant	49,391,665	57

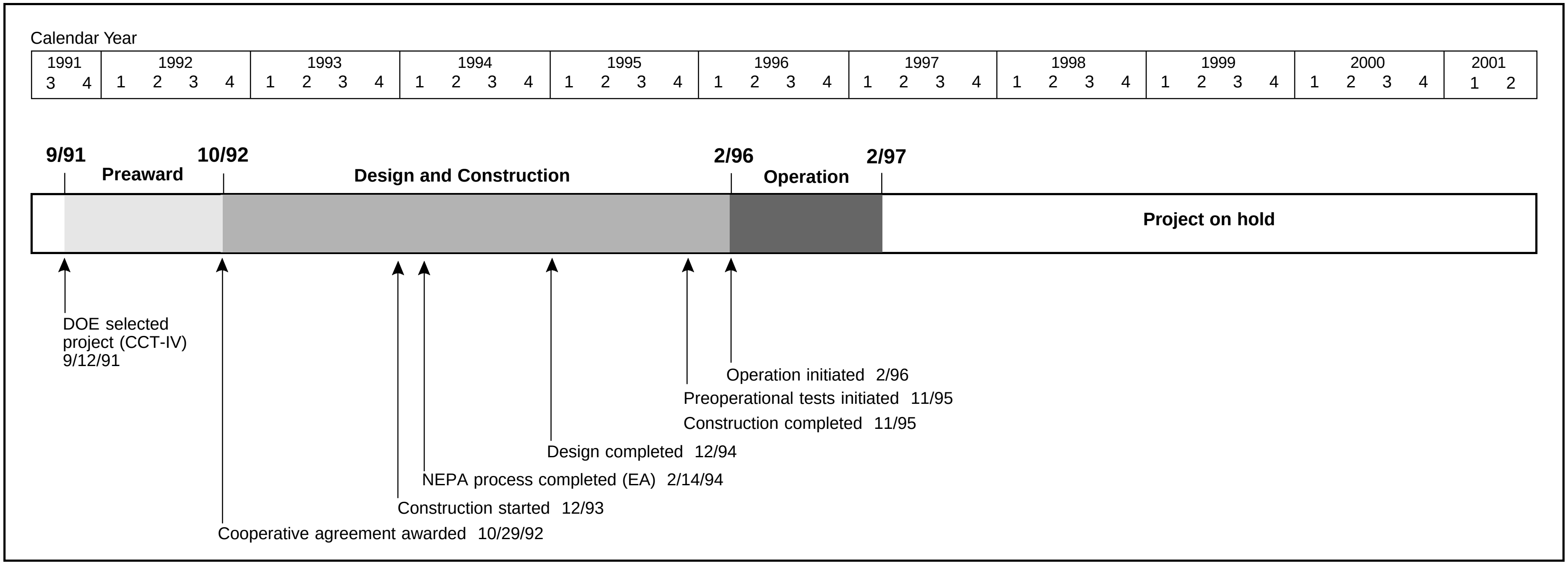
Self-Scrubbing Coal and Carefree Coal are trademarks of Custom Coals International.

Project Objective
To demonstrate advanced coal-cleaning unit processes to produce low-cost compliance coals that can meet the requirements for commercial-scale utility power plants to satisfy provisions of the CAAA.

Technology/Project Description
An advanced coal-cleaning plant has been designed, blending existing and new processes, to produce two types of compliance coals—Carefree Coal™ and Self-Scrubbing Coal™ from high-sulfur bituminous feedstocks.

Carefree Coal™ is produced by breaking and screening run-of-mine coal and by using innovative dense-medium cyclones and finely sized magnetite to remove up to 90% of the pyritic sulfur and most of the ash. Carefree Coal™ is designed to be a competitively priced, high-Btu fuel that can be used without major plant modifications or additional capital expenditures. While many utilities can use Carefree Coal™ to comply with SO_2 emissions limits, others cannot due to the high content of organic sulfur in their coal feedstocks. When compliance coal cannot be produced by reducing pyritic sulfur, Self-Scrubbing Coal™ can be produced to achieve compliance.

Self-Scrubbing Coal™ is produced by taking Carefree Coal™, with its reduced pyritic sulfur and ash content, and adding to it sorbents, promoters, and catalysts. Self-Scrubbing Coal™ is expected to achieve compliance with virtually any U.S. coal feedstock through in-boiler absorption of SO_2 emissions. The reduced ash content of



the Self-Scrubbing Coal™ permits addition of relatively large amounts of sorbent without exceeding ash specifications of boilers or overloading electrostatic precipitators.

Two medium- to high-sulfur coals—Illinois No. 5 (2.7% sulfur) and Lower Freeport (3.9% sulfur)—are being used to produce Self-Scrubbing Coal™. Carefree Coal™ is being made using Lower Kittanning (1.8% sulfur). Lower Kittanning coal is being tested at Martin's Creek Power Station; Illinois No. 5 coal is being tested at Whitewater Valley Generating Station; and Lower Freeport Seam coal is being tested at Ashtabula C.

Project Status/Accomplishments

Start-up began in late December 1995, and the first coal was processed in February 1996. In May 1996, the facility reached its design capacity. Equipment and circuit optimization testing began immediately thereafter and continued throughout 1996.

A Carefree Coal™ test burn (cleaned Lower Kittanning coal) at Martin's Creek Power Station was conducted in mid-November 1996. Although plant optimization was not completed, the overall product made for the test was consistent with the current quality of the plant feed coal. The unit experienced some opacity problems due to the low sulfur in the coal and a marginal electrostatic precipitator.

High organic sulfur in the raw coal created problems with the ability to produce compliance quality clean coal. Further, difficulties with the plant resulted in an excessive amount of material going to the refuse pond, and plant operation was suspended in February 1997.

Financial problems ensued and, despite efforts to resolve the matter, the project was placed in Chapter 11. Due to Custom Coals inability to find a buyer for the facility, the Custom Coals Laurel facility was sold at auction to C.J. Betters Company.

Commercial Applications

Commercialization of Self-Scrubbing Coal™ had the potential of bringing into compliance about 164 million tons/yr of bituminous coal that cannot meet emissions limits through conventional coal-cleaning. This represents more than 38% of the bituminous coal burned in 50-MWe or larger U.S. generating stations.

Advanced Coal Conversion Process Demonstration

Participant
Rosebud SynCoal Partnership (a partnership of Western Energy Company and Western SynCoal)

Additional Team Member
None

Location
Colstrip, Rosebud County, MT (adjacent to Western Energy Company's Rosebud Mine)

Technology
Rosebud SynCoal Partnership's advanced coal conversion process for upgrading low-rank subbituminous and lignite coals

Plant Capacity/Production
45 tons/hr of SynCoal® product (300,000 tons/yr)

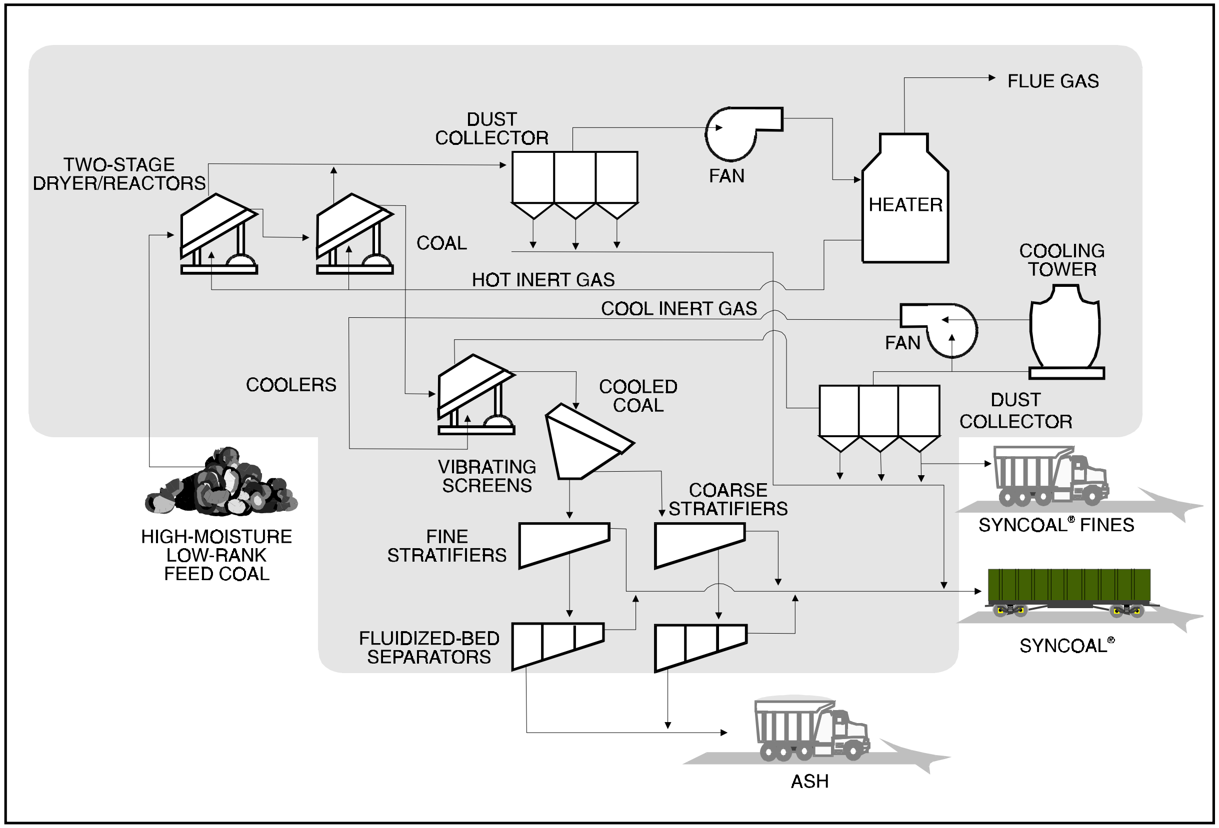
Coal
Powder River Basin subbituminous (Rosebud mine)

Project Funding

Total project cost	$105,700,000	100%
DOE	43,125,000	41
Participant	62,575,000	59

Project Objective
To demonstrate Rosebud SynCoal's advanced coal conversion process to produce SynCoal®, a stable coal product having a moisture content as low as 1%, sulfur content as low as 0.3%, and heating value up to 12,000 Btu/lb.

SynCoal is a registered trademark of the Rosebud SynCoal Partnership.

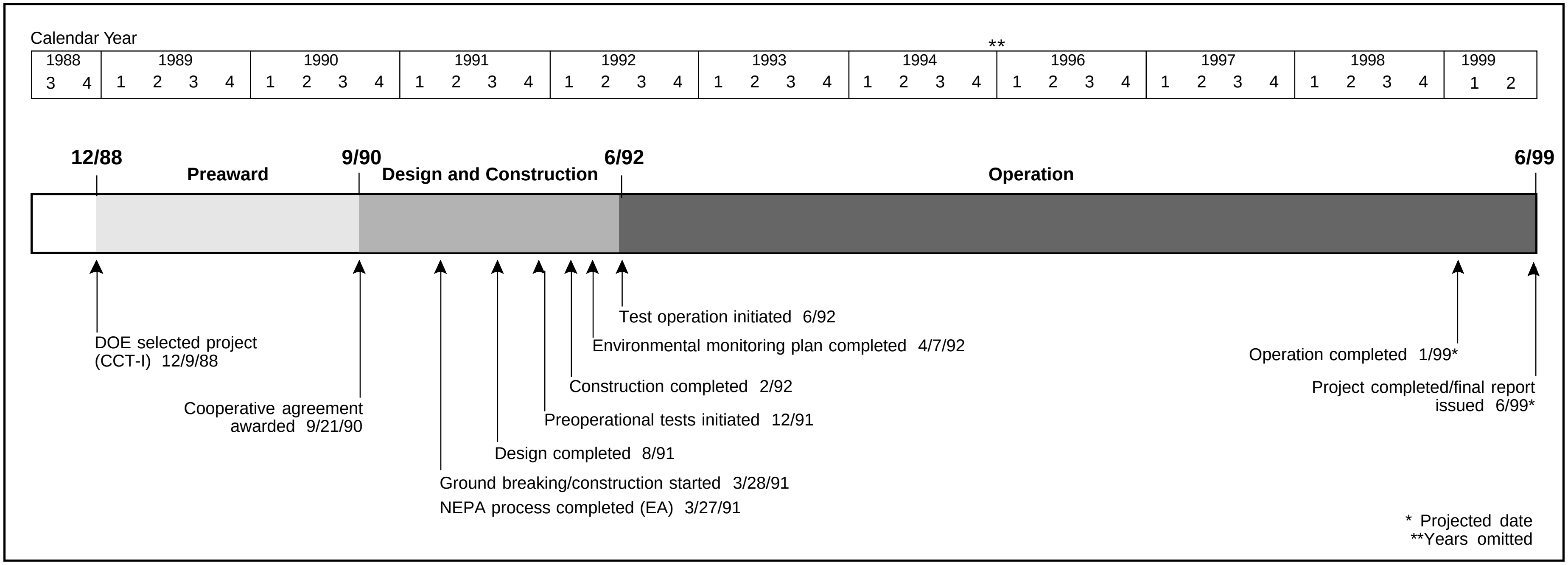


Technology/Project Description
Being demonstrated is an advanced thermal coal conversion process coupled with physical cleaning techniques to upgrade high-moisture, low-rank coals to produce a high-quality, low-sulfur fuel. The coal is processed through two fluidized-bed dryer/reactors that remove loosely held water and then chemically bound water, carboxyl groups, and volatile sulfur compounds. After conversion, the coal is put through a deep-bed stratifier cleaning process to effect separation of the ash.

The technology enhances low-rank western coals, usually with a moisture content of 25–40%, sulfur content of 0.5–1.5%, and heating value of 5,500–9,000 Btu/lb, by producing an upgraded SynCoal® product with a moisture content as low as 1%, sulfur content as low as 0.3%, and heating value up to 12,000 Btu/lb.

The 45-ton/hr unit is located adjacent to a unit train loadout facility at Western Energy Company's Rosebud coal mine in Colstrip, MT. The demonstration plant is one-tenth the size of a commercial facility. However, the process equipment is at 1/3–1/2 commercial scale because a full-sized commercial plant will have multiple process trains.

Project Status/Accomplishments
The Advanced Coal Conversion Process (ACCP) facility continues to process raw subbituminous coal, producing over 1.4 million tons of SynCoal® product to date. Nearly 1.3 million tons has been supplied to industrial applications (primarily cement and lime plants) and utilities. Rosebud SynCoal Partnership has signed a letter agreement between Puget Sound Energy



of Bellevue, Washington and Montana Power Company of Butte, Montana, to design, install, and commission a dedicated pneumatic feed system to supply SynCoal® to Montana Power's 330-MWe Colstrip No. 2. Construction is nearly complete for the Colstrip No. 2 Pneumatic SynCoal® Fuel Project. The plant is continuing to be "cycled," filling the silos and shutting down until Colstrip No. 2 pneumatic feed system is in place (scheduled for January 1999).

A SynCoal® test burn was completed at Montana Power's J.E. Corette in April 1996. The test involved both handling and combustion of SynCoal® in a variety of blends ranging from 15% to 85% SynCoal®. Overall results indicated that a 50% SynCoal®/raw coal blend provides improved results. Sulfur dioxide emissions were reduced by 21% overall, generation increased at normal operating loads, and there was no noticeable impact on NO_x emissions.

In August 1998, Rosebud was granted a six-month no-cost time extension.

Commercial Application

The Rosebud SynCoal ACCP has the potential to enhance the utility and industrial use of low-rank western subbituminous and lignite coals. SynCoal® is an ideal supplement fuel for plants seeking to burn western low-rank coals because it allows a wider range of low-sulfur raw coals to be used to meet more restrictive worldwide emissions guidelines without derating of the units or the addition of costly flue gas desulfurization systems.

The ACCP has potential to convert inexpensive low-sulfur, low-rank coals into valuable carbon-based reducing agents for many metallurgical applications, further helping to reduce world-wide emissions and decrease the U.S. dependence on foreign energy sources.

The ACCP produces a fuel which has a consistently low moisture content, low sulfur content, high heating value, and high volatile content. Because of these characteristics, SynCoal® could have significant

Development of the Coal Quality Expert™

Project completed.

Participants

ABB Combustion Engineering, Inc.
CQ Inc.

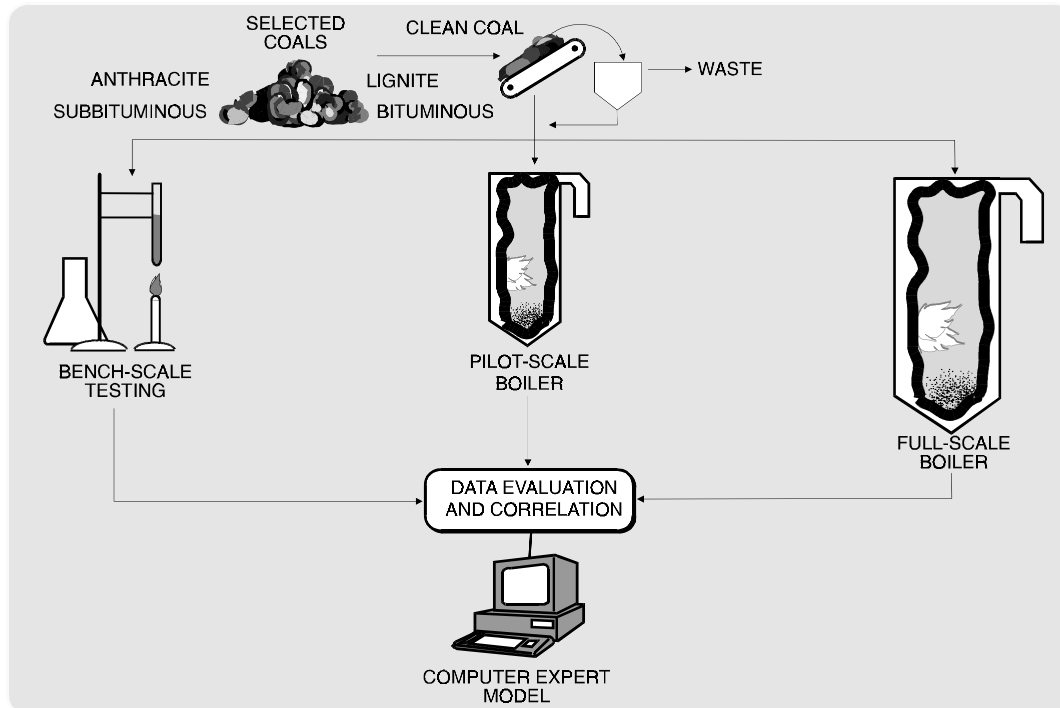
Additional Team Members

Black & Veatch—cofunder and software developer
Electric Power Research Institute—cofunder
The Babcock & Wilcox Company—cofunder and pilot-scale tester
Electric Power Technologies, Inc.—field tester
University of North Dakota, Energy and Environmental Research Center—bench-scale tester
Alabama Power Company—host
Mississippi Power Company—host
New England Power Company—host
Northern States Power Company—host
Public Service Company of Oklahoma—host

Locations

Grand Forks, Grand Forks County, ND (bench tests)
Windsor, Hartford County, CT (bench- and pilot-scale tests)
Alliance, Columbiana County, OH (pilot-scale tests)
Wilsonville, Shelby County, AL (Gatson, Unit No. 5)
Gulfport, Harrison County, MS (Watson, Unit No. 4)
Somerset, Bristol County, MA (Brayton Point, Unit Nos. 2 and 3)
Bayport, Washington County, MN (King Station)
Oologah, Rogers County, OK (Northeastern, Unit No. 4)

Coal Quality Expert, CQE, CQIS, and CQIM are trademarks of the Electric Power Research Institute.



Technology

CQ Inc.'s EPRI Coal Quality Expert™ (CQE™) computer software

Plant Capacity/Production

Full-scale testing took place at six utility sites ranging in size from 250-880-MWe.

Coal

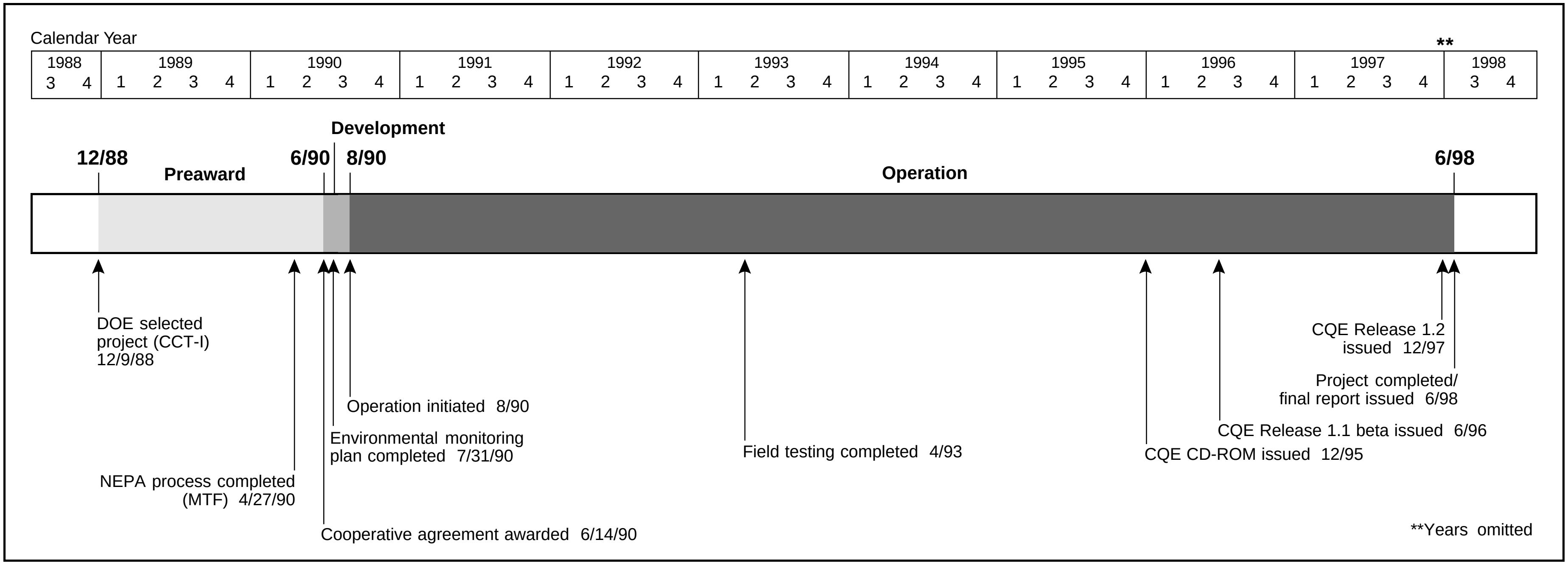
Wide variety of coal blends

Project Funding

Total project cost	$21,746,004	100%
DOE	10,863,911	50
Participants	10,882,093	50

Project Objective

The objective of the project was to provide the utility industry with a PC software program to confidently and inexpensively evaluate the potential for coal-cleaning, blending, and switching options to reduce emissions while producing the lowest cost electricity. Specifically the project was to (1) enhance the existing Coal Quality Information System (CQIS™) database and Coal Quality Impact Model (CQIM™) to allow assessment of the effects of coal-cleaning on specific boiler costs and performance and (2) develop and validate CQE™, a model that allows accurate and detailed prediction of coal quality impacts on total power plant operating cost and performance.



Technology/Project Description

The CQE™ is a software tool that brings a new level of sophistication to fuel decisions by integrating the system-wide impact of fuel purchase decisions on coal-fired power plant performance, emissions, and power generation costs. CQE™ can be used on a stand-alone computer or as a network application for utilities, coal producers, and equipment manufacturers to perform detailed analyses of the impacts of coal quality, capital improvements, operational changes, and/or environmental compliance alternatives on power plant emissions, performance, and production costs. CQE™ can be used as an organized methodology for systematically evaluating all such impacts or it may be used in modules with some default data to perform more strategic or comparative studies.

Project Summary

Background

CQE™ began with EPRI's Coal Quality Impact Model (CQIM™), developed for EPRI by Black & Veatch and introduced in 1989. CQIM™ was endowed with a variety of capabilities, including evaluating Clean Air Act compliance strategies, evaluating bids on coal contracts, conducting test-burn planning and analysis, and providing technical and economic analyses of plant operating strategies. CQE™, which combines CQIM™ with other existing software and databases, extends the art of model-based fuel evaluation established by CQIM™ in three dimensions: new flexibility and application, advanced technical models and performance correlations, and advanced user interface and network awareness.

Algorithm Development

Data derived from bench-, pilot-, and full-scale testing were used to develop the CQE™ algorithms. Bench-scale testing was performed at ABB Combustion Engineering's facilities in Windsor, CT, and the University of North Dakota's Energy and Environmental Research Center in Grand Forks, ND; pilot-scale testing was performed at ABB Combustion Engineering's facilities in Windsor, CT, and Alliance, OH. The six field test sites were Alabama Power's Gatson, Unit No. 5 (880-MWe), Wilsonville, AL; Mississippi Power's Watson, Unit No. 4 (250-MWe), Gulfport, MS; New England Power's Brayton Point, Unit No. 2 (285-MWe) and Unit No. 3 (615-MWe), Somerset, MA; Northern States Power's King Station (560-MWe), Bayport, MN; and Public Service Company of Oklahoma's Northeastern, Unit No. 4 (445-MWe), Oologah, OK.

The six large-scale field tests consisted of burning a baseline coal and an alternate coal over a 2-month period. The baseline coal was used to characterize the operating performance of the boiler. The alternate coal, a blended or cleaned coal of improved quality, was burned in the boiler for the remaining test period.

The baseline and alternate coals for each test site also were burned in bench- and pilot-scale facilities under similar conditions. The alternate coal was cleaned at CQ Inc. to determine what quality levels of clean coal can be produced economically and then transported to the bench- and pilot-scale facilities for testing. All data from bench-, pilot-, and full-scale facilities were evaluated and correlated to formulate algorithms used to develop the model.

CQE™ Capability

The PC-based program evaluates coal quality, transportation system options, performance issues, and alternative emissions control strategies for utility power plants. CQE™ is composed of technical tools to evaluate performance issues, environmental models to evaluate emissions and regulatory issues, and economic models to determine production cost components, including consumables (e.g., fuel, scrubber additives), waste disposal, operation and maintenance, replacement energy costs, and operational and maintenance costs for coal-cleaning processes, power production equipment, and emissions control systems. CQE™ has four main features:

- Fuel Evaluator—Performs system-, plant-, or unit-level fuel quality, economic, and technical assessments.
- Plant Engineer—Provides in-depth performance evaluations with a more focused scope than provided in the Fuel Evaluator.
- Environmental Planner—Provides access to evaluation and presentation capabilities of the Acid Rain Advisor.
- Coal-Cleaning Expert—Establishes the feasibility of cleaning a coal, determines cleaning processes, and predicts associated costs.

Software Description

CQE™ includes more than 100 algorithms based on the data generated in the six full-scale field test.

CQE™'s design philosophy underscores the importance of flexibility by modeling all important power plant equipment and systems and their performance in real-world situations. This level of sophistication allows new applications to be added by assembling a model of how objects interact. Updated information records can be readily shared among all affected users because CQE™ is network-aware, enabling users throughout an organization to share data and results. The CQE™ object-oriented design, coupled with an object database management system, allows different views into the same data. As a result, staff efficiency is enhanced when decisions are made.

CQE™ also can be expanded without major revisions to the system. Object-oriented programming allows new objects to be added and old objects to be deleted or enhanced easily. For example, if modeling advancements are made with respect to predicting boiler ash deposition (i.e., slagging and fouling), the internal calculations of the object that provides these predictions can be replaced or augmented. Other objects affected by ash deposition (e.g., ash collection and disposal systems, soot blower systems) do not need to be altered; thus, the integrity of the underlying system is maintained.

System Requirements

CQE™ currently uses the OS/2 operating system, but the developers are planning to migrate to a Windows-based platform. CQE™ can operate in stand-alone mode on a single computer or on a network. The system requirements for stand-alone operation are listed in Exhibit 5-40. Technical support is available from Black & Veatch for licensed users.

Commercial Applications

The CQE™ system is applicable to all electric power generation plants and large industrial/institutional boilers that burn pulverized coal. Potential users include fuel suppliers, environmental organizations, government and regulatory institutions, and engineering firms. International markets for CQE™ are being explored by both CQ Inc. and Black & Veatch.

EPRI owns the software and distributes CQE™ to EPRI members for their use. CQE™ is available to others in the form of three types of licenses: user, consultant, and commercializer. CQ Inc. and Black & Veatch have each signed commercialization agreements, which give both companies non-exclusive worldwide rights to sell user's licenses and to offer consulting services that include the use of CQE™ software. Two U.S. utilities have been licensed to use copies of CQE™'s stand-alone Acid Rain Advisor. Over 30 U.S. utilities and one U.K. utility have CQE™ through their EPRI membership. Proposals are pending with several non-EPRI-member U.S. and foreign utilities to license their software.

Exhibit 5-40
CQE™ Stand-Alone System Requirements

Item	Minimum	Preferred
Hardware speed	486 PC, 33 Mhz	Pentium PC, market stock
RAM	16 MB	32 MB
Disk space	200 MB	1 GB
Monitor	SVGA color	SVGA color
Graphics card	Capable of 1024x768 mode	Capable of 1024x768 mode
External drives	1.44 MB 3.5-inch; CD-ROM	1.44 MB 3.5-inch; CD-ROM
Mouse	Required	Required
Keyboard	Required	Required
Printer	Access to high-speed printer	Access to laser printer
Operating system	OS/2 Version 2.0	OS/2 WARP (3.0)

The CQE™ team has a Home Page on the World Wide Web (http://www.fuels.bv.com:80/cqe/cqe.htm) and the EPRI Fuels Web Server to promote CQE™, facilitate communications between CQE™ developers and users, and eventually allow software updates to be distributed over the Internet. It also was developed to provide an on-line updatable user's manual. The Home Page also helps attract the interest of international utilities and consulting firms.

CQE™ was recognized by then Energy Secretary Hazel O'Leary and EPRI President Richard Balzhiser in 1996 as the best of nine DOE/EPRI cost-shared utility research and development projects under the "Sustainable Electric Partnership" program.

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Scott M. Smouse, FETC, (412) 892-5725

References

- *Final Report: Development of a Coal Quality Expert*. June 20, 1998.
- Harrison, Clark D., et al. "Recent Experience with the CQE™." *Fifth Annual Clean Coal Technology Conference: Technical Papers*. January 1997.
- *CQE™ Users Manual*, CQE™ Home Page at http://www.fuels.bv.com:80/cqe/cqe.htm.
- *Comprehensive Report to Congress on the Clean Coal Technology Program: Development of the Coal Quality Expert.* ABB Combustion Engineering, Inc., and CQ Inc. Report No. DOE/FE-0174P. U.S. Department of Energy. May 1990. (Available from NTIS as DE90010381.)

▲ CQE™, a PC-based software tool, can be used to determine the complete costs of various fuel options by seamlessly integrating the effects of fuel purchase decisions on power plant performance, emissions, and power generation costs. Portions of the CQE™ User's Manual are available on the Internet.

ENCOAL® Mild Coal Gasification Project

Project completed.

Participant

ENCOAL Corporation (a wholly owned subsidiary of Bluegrass Coal Development Company)

Additional Team Members

Bluegrass Coal Development Company (a wholly owned subsidiary of AEI Resources, Inc.)—cofunder

SGI International—technology developer, owner, licensor

Triton Coal Company (a wholly owned subsidiary of Vulcan Coal Company)— host and coal supplier

The M.W. Kellogg Company—engineer and constructor

Location

Near Gillette, Campbell County, WY (Triton Coal Company's Buckskin Mine site)

Technology

SGI International's Liquids-From-Coal (LFC®) process

Coal

Low-sulfur subbituminous coals

Plant Capacity/Production

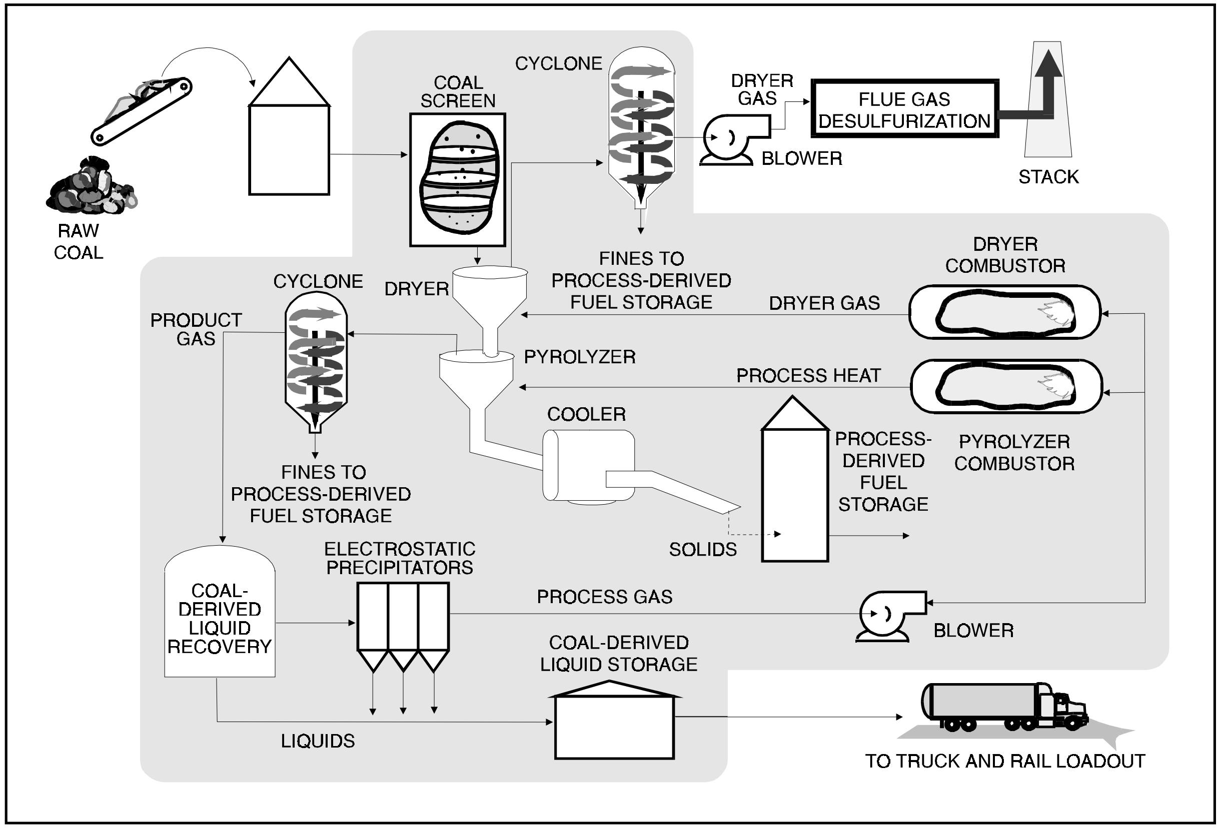
1,000 tons/day of subbituminous coal feed

Project Funding

Total project cost	$90,664,000	100%
DOE	45,332,000	50
Participant	45,332,000	50

Project Objective

To demonstrate the integrated operation of a number of novel processing steps to produce two higher-value fuel forms from mild gasification of low-sulfur subbituminous coal and to provide sufficient products for potential end users to conduct burn tests.



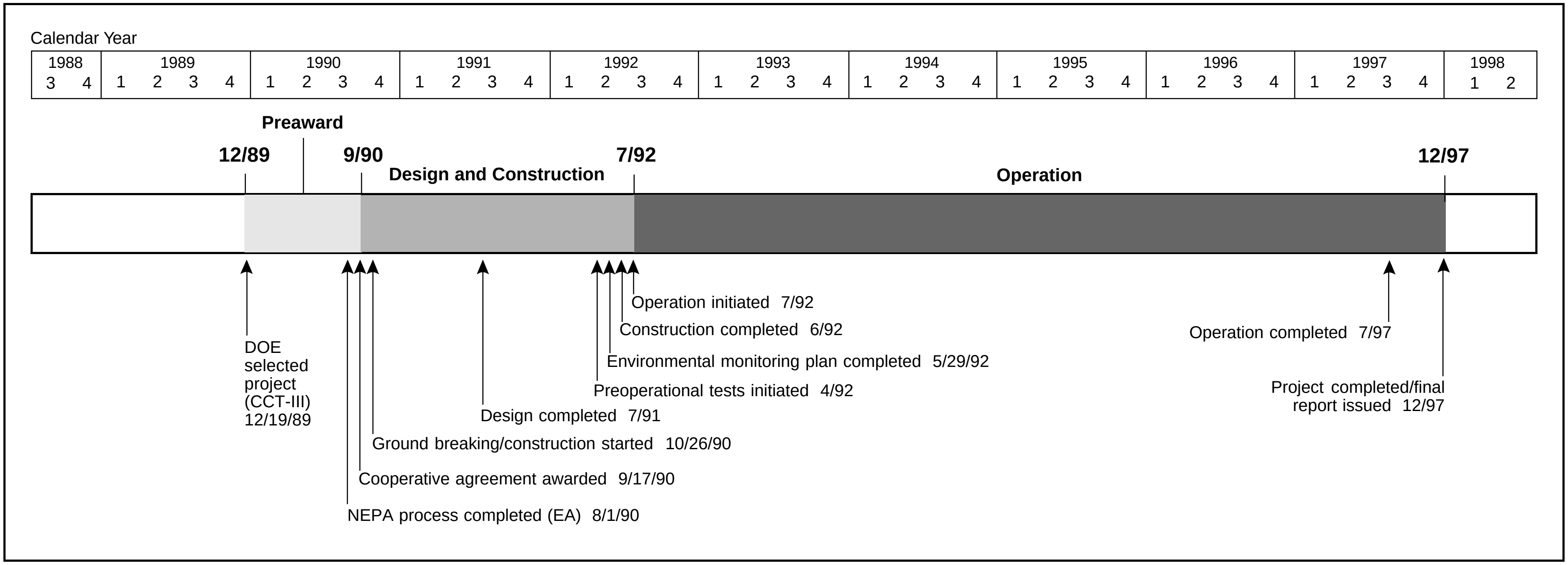
Technology/Project Description

Coal is fed into a rotary grate dryer where it is heated to reduce moisture. The temperature is controlled so that no significant amounts of methane, CO_2, or CO are released. The solids are then fed to the pyrolyzer, where the temperature is about 1,000 °F, and all remaining water is removed. A chemical reaction releases the volatile gaseous material. Solids exiting the pyrolyzer are quenched to stop the pyrolysis reactions.

In the original process, the quench table solids were further cooled in a rotary cooler and transferred to a surge bin. A single 50% flow rate vibrating fluidized-bed (VFB) was added to stabilize the Process-Derived Fuel (PDF®) with respect to oxygen and water. In the VFB, the partially cooled, pyrolyzed solids contact a gas stream containing a controlled amount of oxygen. Termed "oxidative deactivation," a reaction occurs at active surface sites in the particles reducing the tendency for spontaneous ignition.

Following the VFB, the solids are cooled to near atmospheric temperature in an indirect rotary cooler where water is added to rehydrate the PDF®. A patented dust suppressant is added as the PDF® leaves the surge bin. The hot gas produced in the pyrolyzer is sent through a cyclone for removal of the particulates and then cooled in a quench column to stop any additional pyrolysis reactions and to condense the Coal-Derived liquid (CDL®).

ENCOAL, LFC, CDL, and PDF are registered trademarks of SGI and Bluegrass.



Results Summary

Environmental

- The product fuels have been used economically in commercial boilers and furnaces and have reduced SO_2 and NO_x emissions significantly at utility and industrial facilities currently burning high-sulfur bituminous coal or fuel oils.
- One utility reported a 20% reduction in NO_x emissions due to a more stable flame when burning PDF®.
- The PDF® contains 0.36% sulfur with a heat content of 11,100 Btu/lb (compared to 0.45% sulfur and 8,300 Btu/lb for the feed coal).
- The CDL® contains 0.6% sulfur and 140,000 Btu/gal (compared to 0.8% sulfur and 150,000 Btu/gal for No. 6 oil).
- No EPA listed toxins in concentrations anywhere close to federal limits.

Operational

- Almost five years of operating data have been collected for use as a basis for the evaluation and design of a commercial plant.
- Numerous runs exceeding 120 days operation at 90% availability.
- As of July 1997, about 260,000 tons of coal had been processed into 120,000 tons of PDF® and 5,101,000 gallons of CDL®.
- Over 83,500 tons of PDF® have been shipped via 17 unit trains and 1 truck shipment to seven customers in six states. Blends have ranged from 20–100% PDF®.
- Over 200 tank cars of CDL® have been shipped to eight customers in seven states. The largest customer has purchased 101 tank cars and blended the CDL® with its fuel and burned the mixture for process heat.
- PDF® has been tested as a reductant (combined with iron ore) in the direct reduced iron process, and holds promise as a blast furnace injectant.

Economic

- A commercial plant designed to process 15,000-metric-ton/day would cost $475 million (2001 $) to construct with annual operating and maintenance costs of $52 million per year.

Project Summary

Operational

A summary of plant performance is contained in Exhibit 5-41. ENCOAL's first 24-hour run took place in June 1992.

After startup, it became evident that additional processing of the PDF® was necessary. Initially, the PDF® was "finished" by a short exposure to atmospheric conditions in a layered stockpile prior to be reclaimed and shipped, or either blended with run-of-plant PDF®, ROM coal, or the atmosphere stabilized PDF®, but there was a Btu penalty. After considering several alternatives, the VFB was added as part of the deactivation loop.

The VFB was designed to handle only half the ENCOAL plant's designed capacity; when proven, a second VFB was to be installed. Operations became notably smoother and more productive. This was attributable not only to the VFB's improved stabilization of the PDF® and the subsequent increased ease of handling, but also to the replacement of the pyrolyzer sand seal with a water seal and the installation of the process water fines handling system. All these improvements combined to produce a major landmark when ENCOAL® shipped its first train containing PDF® on September 17, 1994 to Western Farmers Electric Cooperative in Hugo, Oklahoma.

ENCOAL met all its goals for its first shipments of PDF® in the Fall of 1994— to demonstrate its ability to coordinate with the Buckskin Mine in loading and shipping consistent blends, to ship PDF® with dust generation comparable to or less than run-of-mine (ROM) Buckskin coal, and to ship PDF® blends that were stable with respect to self heating. Furthermore, ENCOAL demonstrated that PDF® could be transported and delivered to customers using regular commercial equipment. With respect to use, the goal was for customers to burn trial amounts (½ unit train minimum) of PDF® blends with minimal adjustment of equipment. ENCOAL's test burn shipments became international when Japan's Electric Power Development Company evaluated six metric tons of PDF® in 1994. Early 1995 saw much increased plant volume when 13,700 tons of raw coal were processed in a one-month period. Plant availability reached 89%, with downtime attributable to the replacement of the original quench table heat exchanger with a new, high capacity unit.

ENCOAL began shipping unit trains of 100 PDF® for the first time in 1996. By the end of October, two 100 PDF® unit trains were delivered to two separate utilities for test burns. The first was burned in Indiana-Kentucky Electric Cooperative's Clifty Creek Station, which is jointly owned by American Electric Power. The PDF® was blended with Ohio high-sulfur coal at the utility and burned in the Babcock & Wilcox open-path, slag-tap boiler with full instrumentation. Blends tested ranged between 70 and 90% PDF®, and burn results indicated that even with one pulverizer out of service, the unit capacity was increased significantly relative to the base blend. More importantly, there was at least a 20% NO_x reduction due to a more stable flame. Completion of this test burn achieved a primary project milestone of testing PDF® at a major U.S. utility. The remaining 100% PDF® unit train was sent to Northern Indiana Public Service Company and to Union Electric's Sioux Plant near St. Louis, Missouri.

The largest user of the CDL® was Dakota Gas, which purchased 101 tank cars. Dakota Gas blended the CDL® with its fuel and burned the mixture for process heat. A thorough characterization of the CDL® was done by Dakota Gas, for ENCOAL. Tests with a centrifuge successfully removed much of the sediment in the CDL®.

By the end of July, 1997, about 260,000 tons of coal had been processed into 120,000 tons of PDF® and 5,101,000 gallons of CDL®. Over 83,500 tons of PDF® had been shipped to seven customers in six states, as well as 203 tank cars of CDL® to eight customers in seven states.

Stabilization of the PDF® presented challenges to the engineers at ENCOAL. Over 20 different operating conditions were evaluated to enhance the amount of oxygen absorbed in the VFB system. However, VFB deactivation was not complete—stabilization still involved "finishing" using pile layering as well as blending with ROM coal, increased silo retention time, and higher rehydration. This "pile layering" allows the PDF® to react with oxygen and become stable, but is labor intensive and negatively impacts PDF® quality. A stabilization task force composed of private and government engineers and scientists recommended the construction and testing of a Pilot Air Stabilization System (PASS) to complete the oxidative deactivation of PDF® without drying the product. The design and installation of the PASS was completed in November 1995 and the unit operated successfully from November 1995 to January 1996. The PASS processed ½ to 1 ton of solids per hour, 24 hours per day, for 2½ months produc-

Exhibit 5-41
ENCOAL Production

	Pre-VFB 1992	1993	Post-VFB 1994	1995	1996	1997[1]	Sum
Raw Coal Feed (tons)	5,200	12,400	67,500	65,800	68,000	39,340	**258,300**
PDF Produced (tons)	2,200	4,900	31,700	28,600	33,300	19,300	**120,500**
PDF Sold (tons)	0	0	23,700	19,100	32,700	7,400	**82,900**
CDL Produced (bbl)	2,600	6,600	28,000	31,700	32,500	20,300	**121,700**
Hours on Line	314	980	4,300	3,400	3,600	2,603	**15,197**
Average Length of Runs (Days)	2	8	26	38	44	75	

[1]Through June 1997.

ing a stable PDF® that could be stored in uncompacted piles without pile layering.

Environmental

Environmental compliance was an important goal during the demonstration of the LFC® process. Five significant environmental modifications were made at the ENCOAL facility.

Extensive ambient air monitoring work revealed no EPA listed toxins in concentrations anywhere close to federal limits. It was decided, however, to install a vapor recovery system on all process water holding vessels to address an odor problem.

Economic

The "base case" for economics of a commercial plant is the 15,000-metric-ton/day, three-unit North Rochelle LFC® plant, the commercial scale plant proposed by ENCOAL®, with an independent 80-MW cogeneration unit, and no synthetic fuel tax credit (29c tax credit). It is assumed that the cogeneration unit is owned and operated by an independent third-party. The capital cost for a full scale three module LFC® plant is $475 million.

Economic benefits from an LFC® commercial plant are derived from the margin in value between a raw, unprocessed coal and the upgraded products, making an LFC® plant dependent on the cost of feed coal. In fact, this is the largest single operating cost item. The total estimated operating cost is $9.00/ton of feed coal including the cost of feed coal, chemical supplies, maintenance, and labor.

A financial model was constructed using a spreadsheet to evaluate the project's financial viability. The unleveraged Internal Rate of Return (IRR) on the base case of around 15% is encouraging given the project's upfront capital requirements, long construction period, and 30-year project life. The project generates impressive after-tax cash flows (ATCF's) with payback on the base case of less than nine years from plant startup and cumulative ATCF's over 30 years, exceeding $2 billion.

The probability of reaching the 18–20% range for IRR is good, given a combination of lower capital costs and increased revenues. An increase in revenue of 10% coupled with a decrease in capital cost of 10% would provide an unleveraged IRR in excess of 18%.

A possible upside to the base case is use of the nonconventional fuel tax credit commonly referred to as 29c. The addition of 29c to the base case evaluation adds over 15% to the unleveraged IRR, and more than doubles the project net present value.

Commercial Applications

AEI Resources, a unit of Addington Enterprises of Ashland, Kentucky, through its 1998 acquisition of Zeigler Coal Holding Co., holds an undivided and equal interest in the LFC® technology along with SGI International. AEI Resources is the administrative partner responsible for preparation of lease agreements and contracts. In order to determine the viability of potential LFC® plants, five detailed commercial feasibility studies—two Indonesian, one Russian, and two U.S. projects—have been completed. Permitting of a 15,000 metric-ton/day commercial plant in Wyoming is nearly complete.

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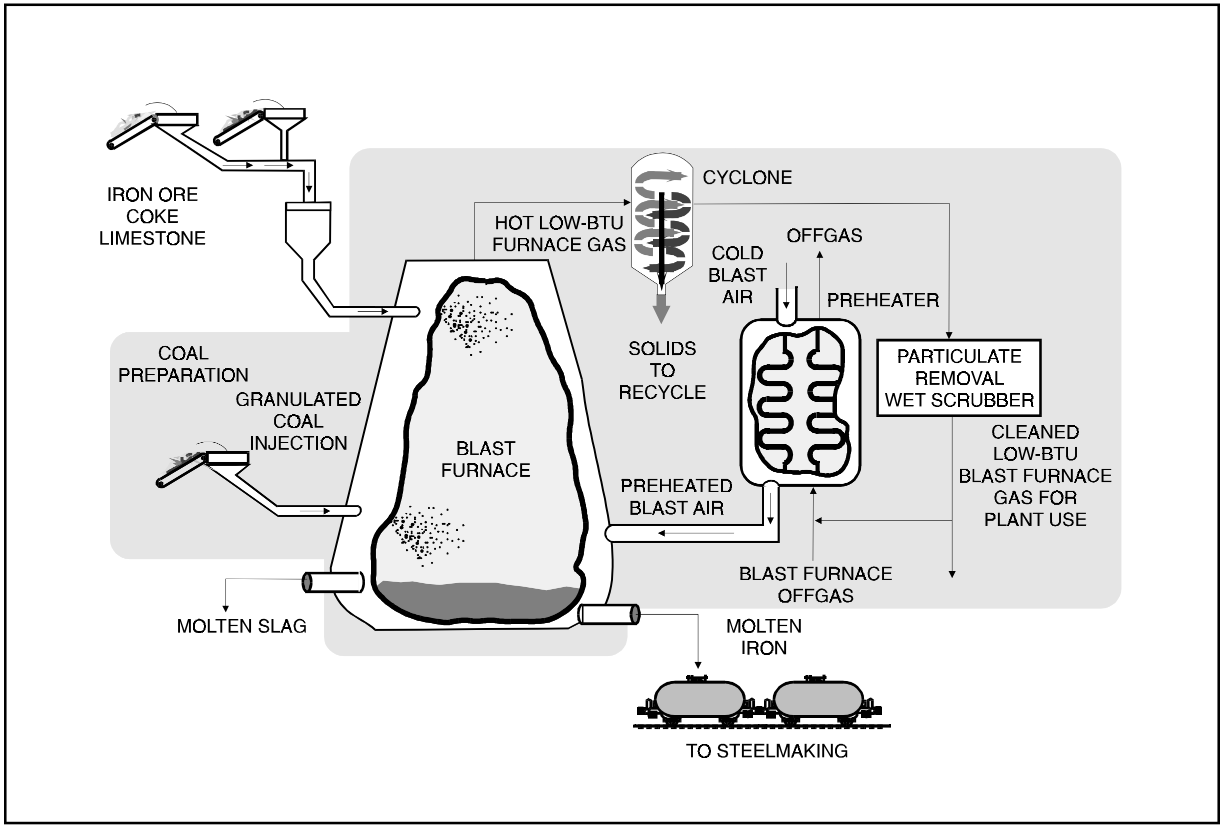
References

- *ENCOAL Mild Coal Gasification Project: Commercial Plant Feasibility Study.* U.S. Department of Energy. September 1997.
- *ENCOAL Mild Gasification Project: Final Design Modifications Report.* U.S. Department of Energy. September 1997.
- *ENCOAL Mild Coal Gasification Project: ENCOAL Project Final Report.* U.S. Department of Energy. September 1997.
- *ENCOAL Mild Coal Gasification Plant: Commercial Plant Feasibility Study.* U.S. Department of Energy. May 1997.

Industrial Applications

Blast Furnace Granular-Coal Injection System Demonstration Project



Participant

Bethlehem Steel Corporation

Additional Team Members

British Steel Consultants Overseas Services, Inc. (marketing arm of British Steel Corporation)—technology owner

CPC-Macawber, Ltd. (formerly named Simon-Macawber, Ltd.)—equipment supplier (world rights to sublicense technology)

Fluor Daniel, Inc.—architect and engineer

ATSI, Inc.—injection equipment engineer (North America technology licensee)

Location

Burns Harbor, Porter County, IN (Bethlehem Steel's Burns Harbor Plant, Blast Furnace Units C and D)

Coal

Eastern bituminous, 0.8–2.8% sulfur; and western subbituminous, 0.4–0.9% sulfur

Technology

British Steel and CPC-Macawber blast furnace granular-coal injection (BFGCI) process

Plant Capacity/Production

7,000 net tons of hot metal (NTHM)/day (each blast furnace)

Project Funding

Total project cost	$194,301,790	100%
DOE	31,824,118	16
Participant	162,477,672	84

Project Objective

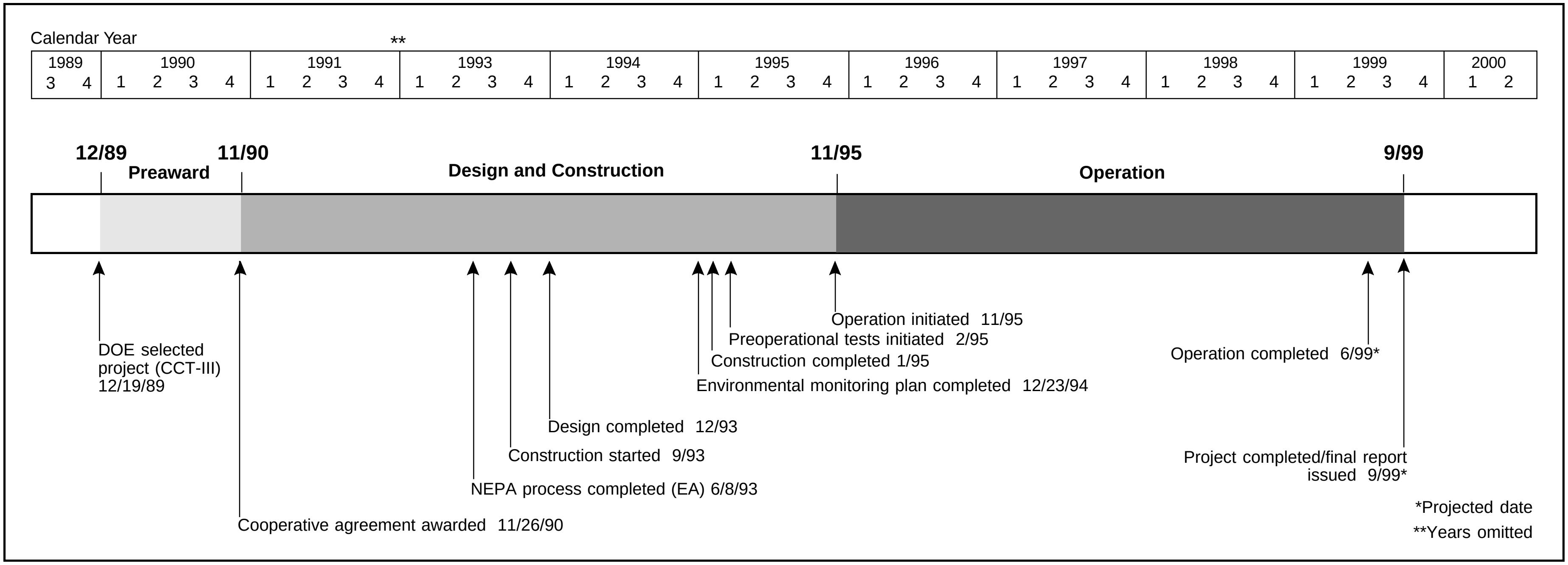
To demonstrate that existing iron-making blast furnaces can be retrofitted with blast furnace granular-coal injection technology; to demonstrate sustained operation with a variety of coal particle sizes, coal injection rates, and coal types; and to assess the interactive nature of these parameters.

Technology/Project Description

In the BFGCI process, either granular or pulverized coal is injected into the blast furnace in place of natural gas or oil as a blast furnace fuel supplement. The coal, along with heated air, is blown into the barrel-shaped section in the lower part of the blast furnace through passages called tuyeres, which creates swept zones in the furnace called raceways. The size of a raceway is important and is dependent upon many factors including temperature. Lowering of a raceway temperature, which can occur with natural gas injection, reduces blast furnace production rates. Coal, with a lower hydrogen content than either natural gas or oil, does not cause as severe a reduction in raceway temperatures. In addition to displacing injected natural gas, the coal injected through the tuyeres displaces coke, the primary blast furnace fuel and reductant (reducing agent), on approximately a pound-for-pound basis. BFGCI technology has significant potential to reduce pollutant emissions and enhance blast furnace production because coke production results in significant emissions of NO_x, SO_2, and air toxics. Coal could replace up to 40% of the coke requirement.

Emissions generated by the blast furnace itself remain virtually unchanged by the injected coal; the gas exiting the blast furnace is cleaned and used in the mill. Sulfur from the coal is removed by the limestone flux and bound up in the slag, which is a salable by-product.

Two high-capacity blast furnaces, Units C and D at Bethlehem Steel's Burns Harbor Plant, were retrofitted



with BFGCI technology. Each unit has a production capacity of 7,000 NTHM/day. The two units use about 2,800 tons/day of coal during full operation. Tests will include eastern bituminous coals with sulfur content of 0.8–2.8% and a western subbituminous coal having 0.4–0.9%.

Project Status/Accomplishments

Early trials comparing high- and low-volatile coals as injectant showed that low-volatile coal replaces more coke and results in better blast furnace operation than high-volatile coal. The replacement ratio was 0.96 pounds of coke replaced for every pound of low-volatile coal used. A major conclusion of the early trials was that granular-coal injection performs very well on large blast furnaces. The low-volatile coals used were Buchanan and Virginia Pocahantas coals (different mines, but same seam and similar properties).

Further trials were conducted on the effect of higher coal ash content on the furnace operation. The baseline coal was the Virginia Pocahantas coal with high carbon and relatively low ash content—both characteristics provide high coke replacement. Three trials were run varying the ash content while keeping all other parameters constant.

The high ash trials revealed that (1) furnace permeability was not changed and a higher ash coal did not have a deleterious effect in the raceway, (2) furnace blast pressure and wind volume were maintained at the base conditions during the trial, (3) furnace production rates were up as delay periods declined during the trial, and (4) hot metal silicon and sulfur content and variability were about the same during all three periods.

Trials were also conducted to determine the coke rate penalty to the blast furnace that results from the use of higher ash injection coal. Corrected coke rates calculated from the trial results reveal that there is a coke rate disadvantage of 3 lb/NTHM for each 1% increase of ash in the injection coal at an injection rate of 260 lb/NTHM.

Sanborn Creek Colorado “B” Seam Coal was selected for trials on western coal. Sufficient granular and pulverized data has been collected on this coal. The data is currently being analyzed.

Commercial Applications

BFGCI technology can be applied to essentially all U.S. blast furnaces. The technology should be applicable to any rank coal commercially available in the United States that has a moisture content no higher than 10%. The environmental impacts of commercial application are primarily indirect and consist of a significant reduction of emissions resulting from diminished coke-making requirements.

The BFGCI technology was developed jointly by British Steel and CPC-Macawber. British Steel has granted exclusive rights to market BFGCI technology worldwide to CPC-Macawber. CPC-Macawber also has the right to sublicense BFGCI rights to other organizations through- out the world. British Steel and CPC-Macawber have recently installed a similar facility at U.S. Steel’s Fairfield blast furnace.

Clean Power from Integrated Coal/Ore Reduction (CPICOR™)

Participant
CPICOR™ Management Company, L.L.C. (a limited liability company composed of subsidiaries of the Geneva Steel Company)

Additional Team Members
Geneva Steel Company—cofunder and host; constructor and operator of unit
PacifiCorp—cofunder

Location
Vineyard, Utah County, UT (Geneva Steel Company's mill)

Technology
HIsmelt® direct ironmaking process

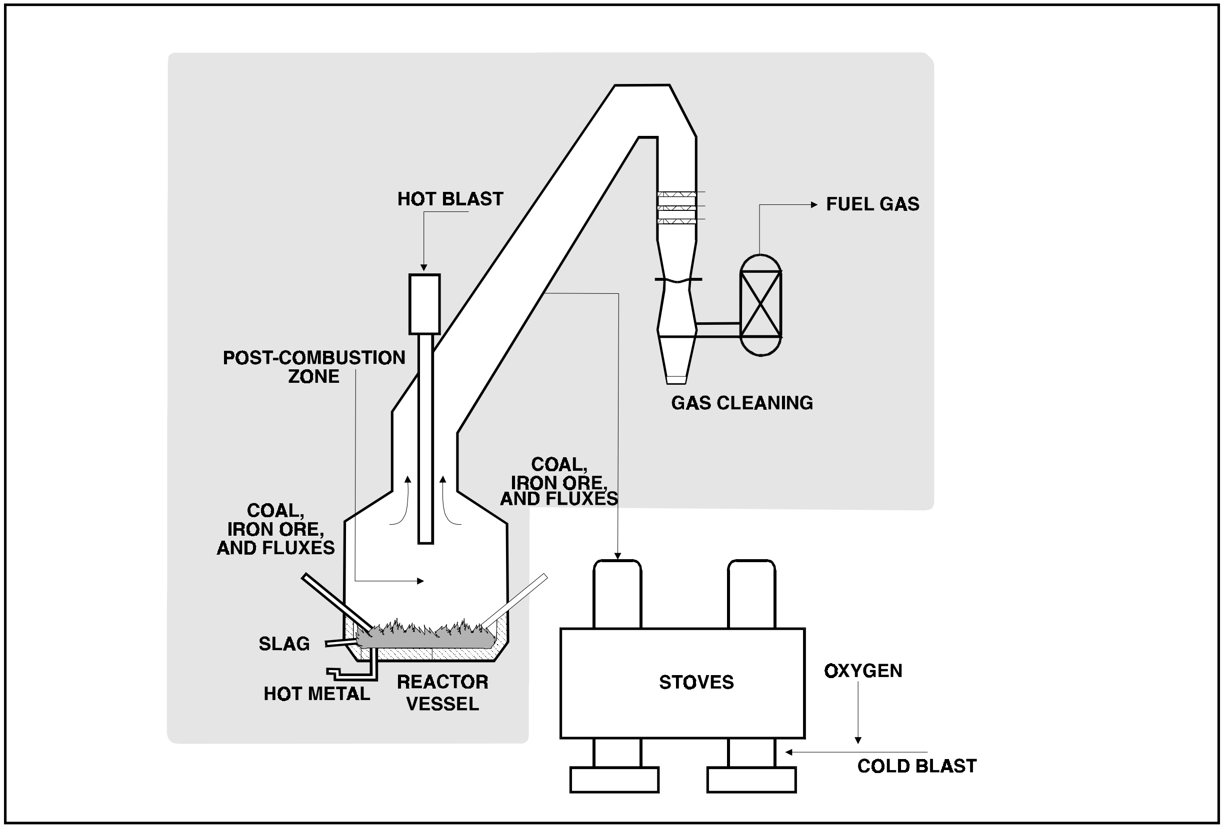
Plant Capacity/Production
3,300 tons/day liquid iron production

Coal
Bituminous, 0.5% sulfur

Project Funding

Total project cost	$1,065,805,000	100%
DOE	149,469,242	14
Participant	916,335,758	86

Project Objective
To demonstrate the integration of a direct iron-making process with the co-production of electricity using various U.S. coals in an efficient and environmentally responsible manner.

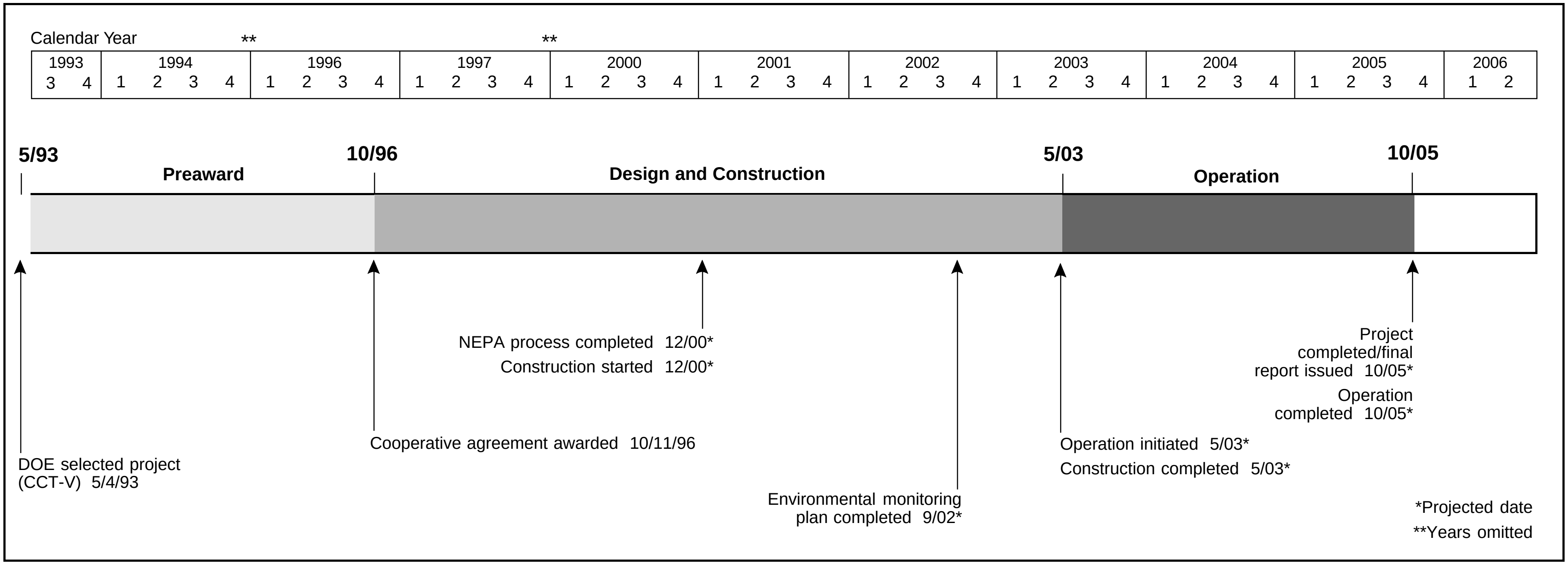


Technology/Project Description
The HIsmelt® process is based on producing hot metal and slag from iron ore fines and non-coking coals. The heart of the process is creating suitable conditions in the HIsmelt® vertical reactor where there is high post-combustion levels with high heat transfer efficiency. The goal is to have sufficient energy input for the reduction and smelting of iron oxides. Tests have consistently demonstrated 60% post-combustion levels with 90% heat transfer efficiency.

The HIsmelt® process uses a vertical smelt reduction reactor, which is a closed molten bath vessel, into which iron ore fines, coal, and fluxes are injected. The coal, which can have a wide range of composition, is injected into the bath where carbon is rapidly dissolved. The dissolved carbon reacts with oxygen (from the injected iron ore) to form carbon monoxide (CO) and metallic iron. Injection gases and evolved CO entrain and propel droplets of slag and molten iron upward into the post combustion zone.

The iron reduction reaction in the molten bath is endothermic; therefore, additional heat must be generated and returned to the bath to sustain the reduction process and maintain an acceptable hot metal temperature. This additional heat is generated by post-combusting the CO and hydrogen (H_2) from the bath with oxygen-enriched hot air blast entering through the central top lance. The heat is absorbed by the metal and slag droplets and returned to the bath as the droplets descend under the gravity. Droplets in contact with the gas in the post-combus-

HIsmelt is a registered trademark of HIsmelt Corporation Pty Limited.
CPICOR is a trademark of the CPICOR™ Management Company,



tion zone absorb heat, but are shrouded during the descent by ascending reducing gases, which together with bath CO, prevent unacceptable levels of slag (FeO).

The molten iron collects in the bottom of the bath and is continuously tapped from the reactor through a fore-hearth, which maintains a constant level of iron in the reactor. Slag, which is periodically tapped through a conventional blast furnace-type tap hole, is used to coat and control the internal cooling system and reduce the heat loss.

Reacted gases, mainly nitrogen (N_2), carbon dioxide (CO_2), CO, H_2, and water vapor (H_2O), exit the vessel. After scrubbing the reacted gases, the cleaned gases will be combusted to produce 170-MWe of power. The cleaned gases can also be used to pre-heat and partially pre-reduce the incoming iron ore.

Project Status/Accomplishments

The cooperative agreement was awarded on October 11, 1996. Permitting and project definition are underway.

CPICOR™ analyzed the global assortment of new direct ironmaking technologies to determine which technology would be most adaptable to western U.S. coals and raw materials. Originally, the COREX® process appeared suitable for using Geneva's local raw materials; however, lack of COREX® plant data on 100% raw coals and ores prevented its application in this demonstration. Thus, CPICOR™ chose to examine alternative direct ironmaking processes. The processes evaluated included: AISI direct ironmaking, DIOS, Romelt, Tecnored, Cyclonic Smelter, and HIsmelt®. The HIsmelt® process appears to offer good economic and operational potential, as well as the prospect of rapid commercialization.

CPICOR™ has completed testing of two U.S. coals at the HIsmelt® pilot plant near Perth, Australia.

Commercial Applications

The HIsmelt® technology is a direct replacement for existing blast furnace and coke-making facilities with additional potential to produce steam for power production. Of the existing 79 coke oven batteries, half are 30 years of age or older and are due for replacement or major rebuilds. There are about 60 U.S. blast furnaces, all of which have been operating for more than 10 years, with some originally installed up to 90 years ago. HIsmelt® represents a viable option as a substitute for conventional ironmaking technology.

The HIsmelt® process is ready for demonstration. Two pilot plants have been built, one in Germany in 1984 and one in Kwinana, Western Australia in 1991. Through test work in Australia, the process has been proven—operational control parameters have been identified and

Advanced Cyclone Combustor with Internal Sulfur, Nitrogen, and Ash Control

Project completed.

Participant
Coal Tech Corporation

Additional Team Members
Commonwealth of Pennsylvania, Energy Development Authority—cofunder
Pennsylvania Power and Light Company—supplier of test coals
Tampella Power Corporation—host

Location
Williamsport, Lycoming County, PA (Tampella Power Corporation's boiler manufacturing plant)

Technology
Coal Tech's advanced, air-cooled, slagging combustor

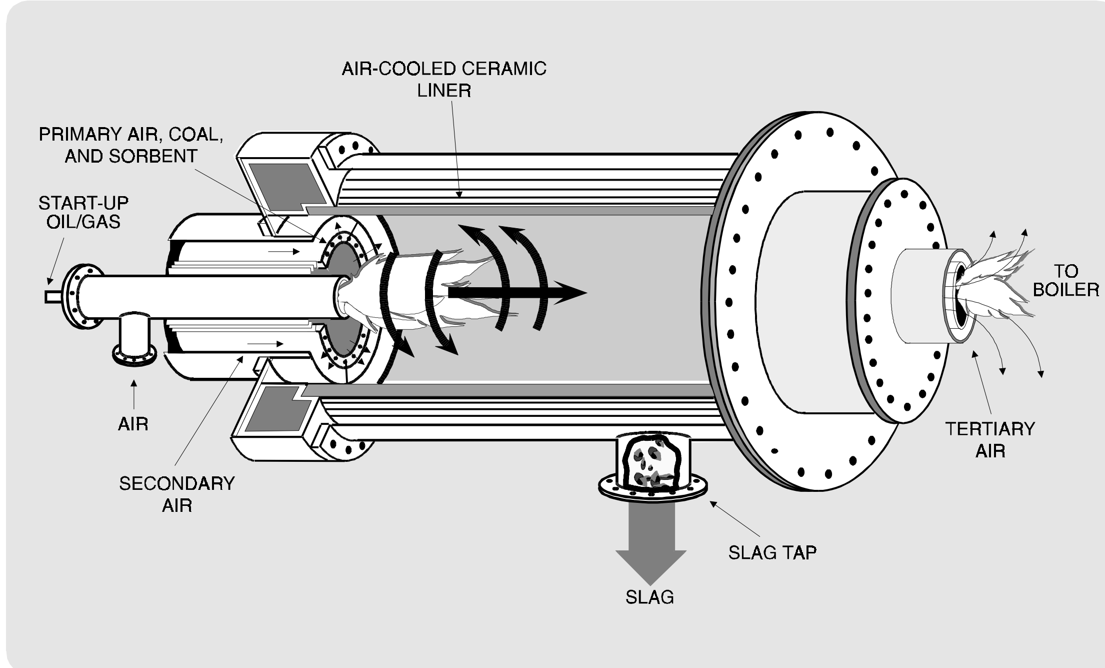
Plant Capacity/Production
23 x 10^6 Btu/hr

Coal
Pennsylvania bituminous, 1.0–3.3% sulfur

Project Funding

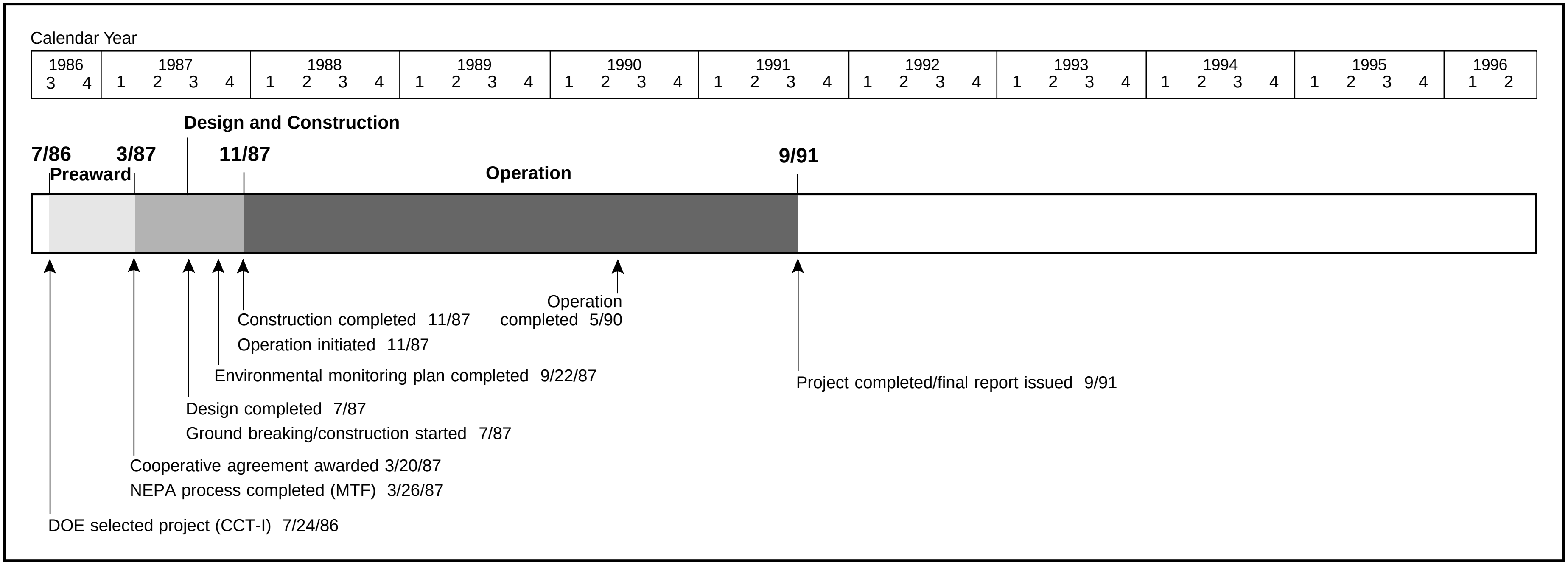
Total project cost	$984,394	100%
DOE	490,149	50
Participant	494,245	50

Project Objective
To demonstrate that an advanced cyclone combustor can be retrofitted to an industrial boiler and that it can simultaneously remove up to 90% of the SO_2 and 90–95% of the ash within the combustor and reduce NO_x to 100 ppm.



Technology/Project Description
Coal Tech's horizontal cyclone combustor is internally lined with an air-cooled ceramic that is air-cooled. Pulverized coal, air, and sorbent are injected tangentially toward the wall through tubes in the annular region of the combustor to cause cyclonic action. In this manner, coal-particle combustion takes place in a swirling flame in a region favorable to particle retention in the combustor. Secondary air is used to adjust the overall combustor stoichiometry. Tertiary air is injected at the combustor/boiler interface. The ceramic liner is cooled by the secondary air and maintained at a temperature high enough to keep the slag in a liquid, free-flowing state. The secondary air is preheated by the combustor walls to attain efficient combustion of the coal particles in the fuel-rich combustor. Fine coal pulverization allows combustion of most of the coal particles near the cyclone wall. The combustor was designed to retain a high percentage of the ash and sorbent fed to the combustor as slag. For NO_x control, the combustor is operated fuel rich, with final combustion taking place in the boiler furnace to which the combustor is attached. SO_2 is captured by injection of limestone into the combustor. The cyclonic action inside the combustor forces the coal ash and sorbent to the walls where it can be collected as liquid slag. Under optimum operating conditions, the slag contains a significant fraction of vitrified coal sulfur. Downstream sorbent injection into the boiler provides additional sulfur removal capacity.

In Coal Tech's demonstration, an advanced, air-cooled, cyclone coal combustor was retrofitted to a 23 x 10^6 Btu/hr, oil-designed package boiler located at the



Tampella Power Corporation boiler factory in Williamsport, PA.

Results Summary

Environmental

- SO_2 removal efficiencies of over 80% were achieved with sorbent injection in the furnace at various calcium-to-sulfur (Ca/S) molar ratios.
- SO_2 removal efficiencies up to 58% were achieved with sorbent injection in the combustor at a Ca/S molar ratio of 2.0.
- A maximum of 1/3 of the coal's sulfur was retained in the dry ash removed from the combustor (as slag) and furnace hearth.
- At most, 11% of the coal's sulfur was retained in the slag rejected through the combustor's slag tap.
- NO_x emissions were reduced to 184 ppm by the combustor and furnace and to 160 ppm with the addition of a wet particulate scrubber.
- Combustor slag was essentially inert.
- Ash/sorbent retention in the combustor as slag averaged 72% and ranged from 55–90%. Under more fuel lean conditions, retention averaged 80%.
- Meeting local particulate emissions standards required the addition of a wet venturi scrubber.

Operational

- Combustion efficiencies of over 99% were achieved.
- A 3-to-1 combustor turndown capability was demonstrated. Protection of combustor refractory with slag was shown to be possible.
- A computer-controlled system for automatic combustor operation was developed and demonstrated.

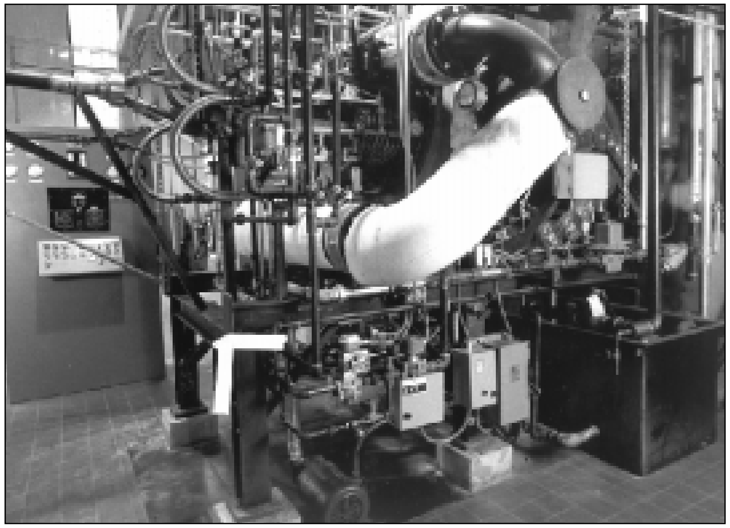
Economic

- Because the technology failed to meet commercialization criteria, economics were not developed during the demonstration. However, subsequent efforts indicate that incremental capital costs for installing the coal combustor in lieu of oil or gas systems are \$100–\$200/kW.

Project Summary

The novel features of Coal Tech's patented ceramic-lined, slagging cyclone combustor included its air-cooled walls and environmental control of NO_x, SO_2, and solid waste emissions. Air cooling took place in a very compact combustor, which could be retrofitted to a wide range of industrial and utility boiler designs without disturbing the boiler's water-steam circuit. In this technology, NO_x reduction was achieved by staged combustion, and SO_2 was captured by injection of limestone into the combustor and/or boiler. Critical to combustor performance was removal of ash, as slag, which would otherwise erode boiler tubes. This was particularly important in oil furnace retrofits where tube spacing is tight (made possible by the low-ash content of oil-based fuels).

The test effort consisted of 800 hours of operation, including five individual tests, each of four days duration. An additional 100 hours of testing was performed as part of a separate ash vitrification test. Test results obtained during operation of the combustor indicated that Coal Tech attained most of the objectives contained in the cooperative agreement. About eight different Pennsylvania bituminous coals with sulfur contents ranging from 1.0–3.3% and volatile matter contents ranging from 19–37% were tested.



▲ The slagging combustor, associated piping, and control panel for Coal Tech's advanced ceramic-lined slagging combustor are shown.

Environmental Performance

A maximum of over 80% SO_2 reduction measured at the boiler outlet stack was achieved using sorbent injection in the furnace at various Ca/S molar ratios. A maximum SO_2 reduction of 58% was measured at the stack with limestone injection into the combustor at a Ca/S molar ratio of 2. A maximum of 1/3 of the coal's sulfur was retained in the dry ash removed from the combustor and furnace hearths, and as much as 11% of the coal's sulfur was retained in the slag rejected through the slag tap. Additional sulfur retention in the slag is possible by increasing the slag flow rate and further improving fuel-rich combustion and sorbent-gas mixing.

With fuel-rich operation of the combustor, a three-fourths reduction in measured boiler outlet stack NO_x was obtained, corresponding to 184 ppm. An additional 5–10% reduction was obtained by the action of the wet particulate scrubber, resulting in atmospheric NO_x emissions as low as 160 ppm.

All the slag removed from the combustor produced trace metal leachates well below EPA's Drinking Water Standard.

Total ash/sorbent retention as slag in the combustor under efficient combustion operating conditions averaged 72% and ranged from 55–90%. Under more fuel-lean conditions, the slag retention averaged 80%. In post-CCT project tests on flyash vitrification in the combustor, modifications to the solids injection system and increases in the slag flow rate produced substantial increases in the slag retention rate. To meet local stack particulate emission standards, a wet venturi particulate scrubber was installed at the boiler outlet.

Operational Performance

Combustion efficiencies exceeded 99% after proper operating procedures were achieved. Combustor turndown to 6 x 10^6 Btu/hr from a peak of 19 x 10^6 Btu/hr (or a 3-to-1 turndown) was achieved. The maximum heat input during the tests was around 20 x 10^6 Btu/hr, even though the combustor was designed for 30 x 10^6 Btu/hr and the boiler was thermally rated at around 25 x 10^6 Btu/hr. This situation resulted from facility limits on water availability for the boiler and for cooling the combustor. In fact, due to the lack of sufficient water cooling, even 20 x 10^6 Btu/hr was borderline, so that most of the testing was conducted at lower rates.

Different sections of the combustor had different materials requirements. Suitable materials for each section were identified. Also, the test effort showed that operational procedures were closely coupled with materials durability. As an example, by implementing certain procedures, such as changing the combustor wall temperature, it was possible to replenish the combustor refractory wall thickness with slag produced during combustion rather than by adding ceramic to the combustor walls.

The combustor's total operating time during the life of the CCT project was about 900 hours. This included approximately 100 hours of operation in two other flyash vitrification tests projects. Of the total time, about one-third was with coal; about 125 tons of coal were consumed.

Developing proper combustor operating procedures was also an objective. Not only were procedures for properly operating an air-cooled combustor developed, but the entire operating data base was incorporated into a computer-controlled system for automatic combustor operation.

Commercial Applications

In conclusion, the goal of this project was to validate the performance of the air-cooled combustor at a commercial scale. While the combustor was not yet fully ready for sale with commercial guarantees, it was believed to have commercial potential. Subsequent work was undertaken, which has brought the technology close to commercial introduction.

Contacts

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References

- *The Coal Tech Advanced Cyclone Combustor Demonstration Project—A DOE Assessment.* Report No. DOE/PC/79799-T1. U.S. Department of Energy. May 1993. (Available from NTIS as DE93017043.)
- *The Demonstration of an Advanced Cyclone Coal Combustor, with Internal Sulfur, Nitrogen, and Ash Control for the Conversion of a 23 MMBtu/Hour Oil Fired Boiler to Pulverized Coal; Vol. 1: Final Technical Report; Vol. 2: Appendixes I–V; Vol. 3: Appendix VI.* Coal Tech Corporation. August 1991. (Available from NTIS as DE92002587 and DE92002588.)
- *Comprehensive Report to Congress on the Clean Coal Technology Program: Advanced Cyclone Combustor with Internal Sulfur, Nitrogen, and Ash Control*. Coal Tech Corporation. Report No. DOE/FE-0077. U.S. Department of Energy. February 1987. (Available from NTIS as DE87005804.)

▲ Coal Tech's slagging combustor demonstrated the capability to retain, as slag, a high percentage of the non-fuel components injected into the combustor. The slag, shown on the conveyor, is essentially an inert glassy by-product with value in the construction industry as aggregate or in the manufacture of abrasives.

Cement Kiln Flue Gas Recovery Scrubber

Project completed.

Participant
Passamaquoddy Tribe

Additional Team Members
Dragon Products Company—project manager and host
HPD, Incorporated—designer and fabricator of tanks and heat exchanger
Cianbro Corporation—constructor

Location
Thomaston, Knox County, ME (Dragon Products Company's coal-fired cement kiln)

Technology
Passamaquoddy Technology Recovery Scrubber™

Plant Capacity/Production
1,450 tons/day of cement; 250,000 scfm of kiln gas; and up to 274 tons/day of coal

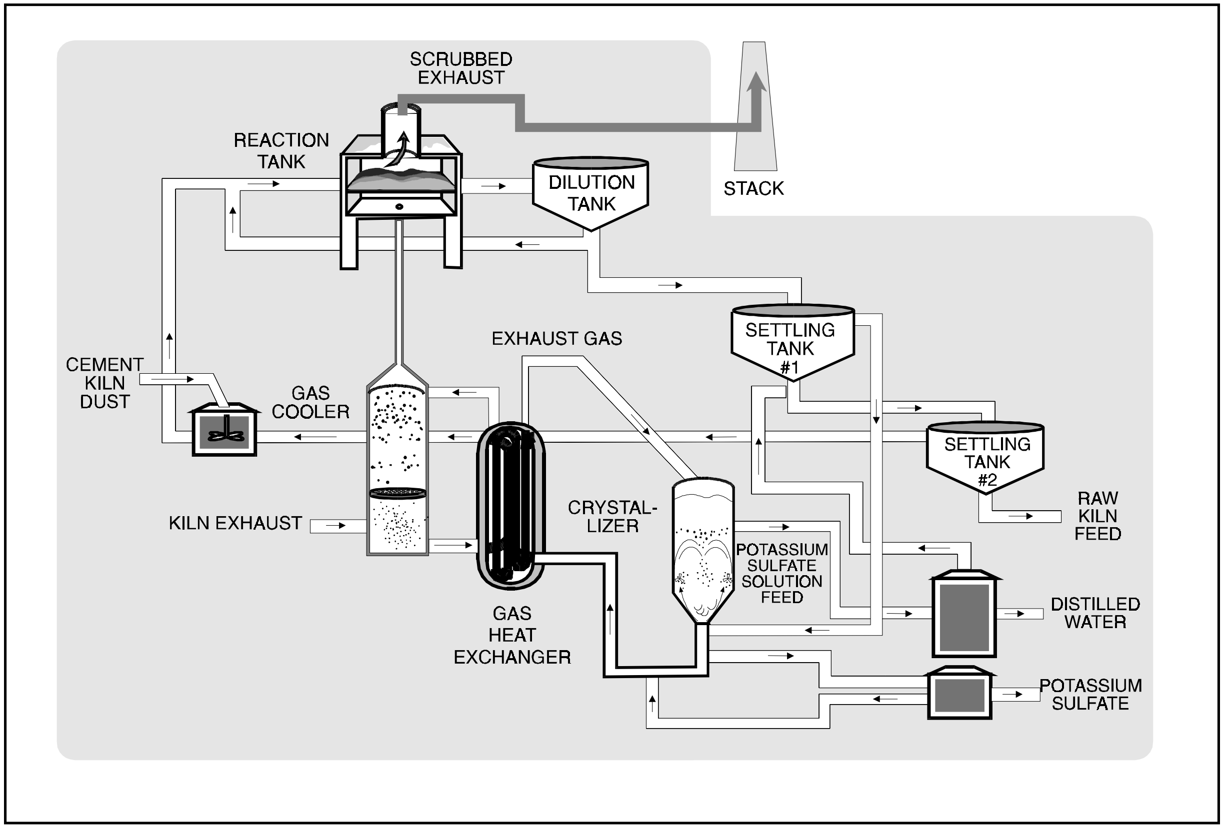
Coal
Pennsylvania bituminous, 2.5–3.0% sulfur

Project Funding

Total project cost	$17,800,000	100%
DOE	5,982,592	34
Participant	11,817,408	66

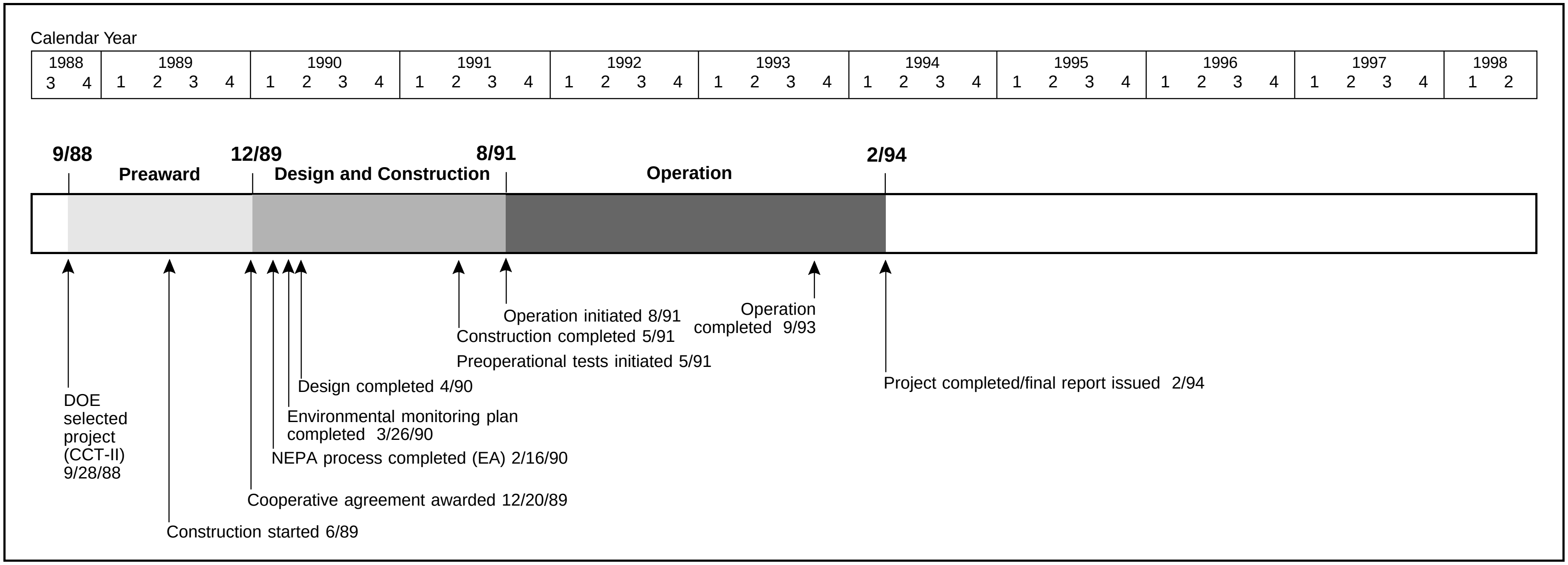
Project Objective
To retrofit and demonstrate a full-scale industrial scrubber and waste recovery system for a coal-burning wet process cement kiln using waste dust as the reagent to accomplish 90–95% SO_2 reduction using high-sulfur eastern coals; and to produce a commercial by-product, potassium-based fertilizer byproducts.

Passamaquoddy Technology Recovery Scrubber is a trademark of the Passamaquoddy Tribe.



Technology/Project Description
The Passamaquoddy Technology Recovery Scrubber™ uses cement kiln dust (CKD), an alkaline-rich (potassium) waste, to react with the acidic flue gas. This CKD, representing about 10% of the cement feedstock otherwise lost as waste, is formed into a water-based slurry and mixed with the flue gas as the slurry passes over a perforated tray that enables the flue gas to percolate through the slurry. The SO_2 in the flue gas reacts with the potassium to form potassium sulfate, which stays in solution and remains in the liquid as the slurry undergoes separation into liquid and solid fractions. The solid fraction, in thickened slurry form and freed of the potassium and other alkali constituents, is returned to the kiln as feedstock (it is the alkali content that makes the CKD unusable as feedstock). No dewatering is necessary for the wet process used at the Dragon Products Plant. The liquid fraction is passed to a crystallizer that uses waste heat in the flue gas to evaporate the water and recover dissolved alkali metal salts. A recuperator lowers the incoming flue gas temperature to prevent slurry evaporation, enables the use of low-cost fiberglass construction material, and provides much of the process water through condensation of exhaust gas moisture.

The Passamaquoddy Technology Recovery Scrubber™ was constructed at the Dragon Products Company's cement plant in Thomaston, ME, a plant that can process approximately 450,000 tons/yr of cement. The process was developed by the Passamaquoddy Indian Tribe while it was seeking ways to solve landfill problems, which resulted from the need to dispose of CKD from the cement-making process.



Results Summary

Environmental

- The SO_2 removal efficiency averaged 94.6% during the last several months of operation and 89.2% for the entire operating period.
- The NO_x removal efficiency averaged nearly 25% during the last several months of operation and 18.8% for the entire operating period.
- All of the 250-ton/day CKD waste produced by the plant was renovated and reused as feedstock. This resulted in reducing the raw feedstock requirement by 10% and eliminating solid waste disposal costs.
- Particulate emission rates of 0.005–0.007 gr/scf, about 1/10 that allowed for cement kilns, were achieved with dust loadings of approximately 0.04 gr/scf.
- Pilot testing conducted at U.S. Environmental Protection Agency laboratories under Passamaquoddy Technology, L.P. sponsorship showed 98% HCl removal.
- On three different runs, VOC (as represented by alpha-pinene) removal efficiencies of 72.3, 83.1, and 74.5% were achieved.
- A reduction of approximately 2% in CO_2 emissions was realized through recycling of the CKD.

Operational

- During the last operating interval, April to September 1993, recovery scrubber availability (discounting host site downtime) steadily increased from 65% in April 1993 to 99.5% in July 1993.

Economic

- Capital costs are approximately $10,090,000 (1990 $) for a recovery scrubber to control emissions from a 450,000-ton/yr wet process plant, with a simple payback estimated in 3.1 years. Operating and maintenance costs, estimated at $500,000/yr, plus capital and interest costs, are generally offset by avoided costs associated with fuel, feedstock, and waste disposal and with revenues from the sale of fertilizer.

Project Summary

The Passamaquoddy Technology Recovery Scrubber™ is a unique process that achieves efficient acid gas and particulate control through effective contact between flue gas and a potassium-rich slurry composed of waste kiln dust. Flue gas passes through the slurry as it moves over a special sieve tray. This results in high SO_2 and particulate capture, some NO_x reduction, and sufficient uptake of the potassium (an unwanted constituent in cement) to allow the slurry to be recycled as feedstocks. Waste cement kiln dust, exhaust gases (including waste heat), and wastewater are the only inputs to the process. Renovated cement kiln dust, potassium-based fertilizer, scrubbed exhaust gas, and distilled water are the only proven outputs. There is no waste.

The scrubber was evaluated over three basic operating intervals dictated by winter shutdowns for maintenance and inventory and 14 separate operating periods (within these basic intervals) largely determined by unforeseen host-plant maintenance and repairs and a depressed cement market. Over the period August 1991 to September 1993, more than 5,300 hours was logged, 1,400 hours in the first operating interval, 1,300 hours in the second interval, and 2,600 hours in the third interval. Sulfur loadings varied significantly over the operating periods due to variations in feedstock and operating conditions.

Operational Performance

Several design problems were discovered and corrected during start-up. No further problems were experienced in these areas during actual operation.

Two problems persisted into the demonstration period. The mesh-type mist eliminator, which was installed to prevent slurry entrainment in the flue gas, experienced plugging. Attempts to design a more efficient water spray for cleaning failed. However, replacement with a chevron-type mist eliminator prior to the third operating interval was effective. Potassium sulfate pelletization proved to be a more difficult problem. The cause was eventually isolated and found to be excessive water entrainment due to carry-over of gypsum and syngenite. Hydroclones were installed in the crystallizer circuit to separate the very fine gypsum and syngenite crystals from the much coarser potassium sulfate crystals. Although the correction was made, it was not in time to realize pellet production during the demonstration period. After all modifications were completed, the recovery scrubber entered into the third and final operating interval—April to September 1993. During this interval, recovery scrubber availability (discounting host site downtime) steadily increased from 65% in April to 99.5% in July.

Environmental Performance

An average 250 tons/day of CKD waste generated by the Dragon Products plant was used as the sole reagent in the recovery scrubber to treat approximately 250,000 scfm of flue gas. All the CKD, or approximately 10 tons/hr, were renovated and returned to the plant as feedstock and mixed with about 90 tons/hr of fresh feed to make up the required 100 tons/hr. The alkali in the CKD was converted to potassium-based fertilizer, eliminating all solid waste. Exhibit 5-42 lists the number of hours per operating period, SO_2 and NO_x inlet and outlet readings in pounds per hour, and removal efficiency as a percentage for each operating period.

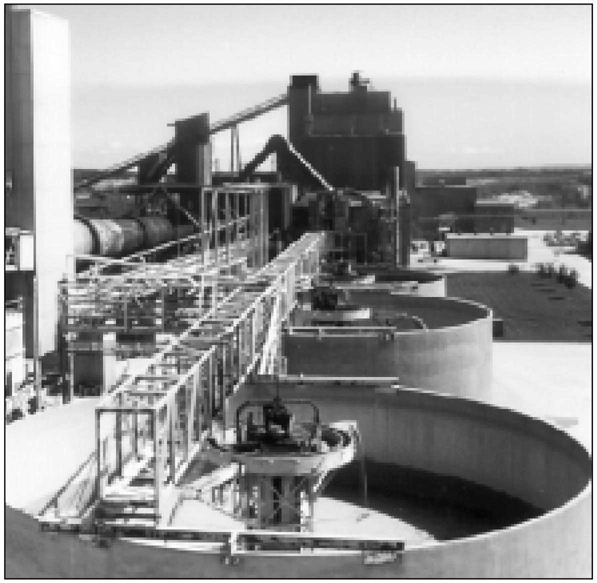
Average removal efficiencies during the demonstration period were 89.2% for SO_2 and 18.8% for NO_x emissions. No definitive explanation for the NO_x control mechanics was available at the conclusion of the demonstration.

Aside from the operating period emissions data, an assessment was made of inlet SO_2 load impact on removal efficiency. For SO_2 inlet loads in the range of 100 lb/hr or less, recovery scrubber removal efficiency averaged 82.0%. For SO_2 inlet loads in the range of 100–200 lb/hr, removal efficiency increased to 94.1% and up to 98.5% for loads greater than 200 lb/hr.

In compliance testing for the State of Maine's Department of Environmental Quality, the recovery scrubber was subjected to dust loadings of approximately 0.04 gr/scf and demonstrated particulate emission rates of 0.005–0.007 gr/scf—less than 1/10 the current allowable limit.

Exhibit 5-42
Summary of Emissions and Removal Efficiencies

Operating Period	Operating Time (hr)	Inlet (lb/hr)		Outlet (lb/hr)		Removal Efficiency (%)	
		SO_2	NO_x	SO_2	NO_x	SO_2	NO_x
1	211	73	320	10	279	87.0	12.8
2	476	71	284	11	260	84.6	08.6
3	464	87	292	13	251	85.4	14.0
4	259	131	252	16	165	87.6	34.5
5	304	245	293	28	243	88.7	17.1
6	379	222	265	28	208	87.4	21.3
7	328	281	345	28	244	90.1	29.3
8	301	124	278	10	188	91.8	32.4
9	314	47	240	7	194	85.7	19.0
10	402	41	244	6	218	86.1	10.5
11	460	36	315	6	267	83.4	15.0
12	549	57	333	2	291	95.9	12.4
13	464	86	288	4	223	95.0	22.6
14	405	124	274	9	199	92.4	27.4
Total	5,316						
Weighted Average		**109**	**289**	**12**	**234**	**89.2**	**18.8**



▲ The Passamaquoddy Technology Recovery Scrubber™ was successfully demonstrated at Dragon Products Company's cement plant in Thomaston, ME.

Economic Performance

The estimated "as-built" capital cost to reconstruct the Dragon Products prototype, absent the modifications, is $10,090,000 in 1990 dollars.

Annual operating and maintenance costs are estimated at $500,000. Long-term annual maintenance costs are estimated at $150,000. Power costs, estimated at $350,000/yr, are the only significant operating costs. There are no costs for reagents or disposal, and no dedicated staffing or maintenance equipment are required.

Considering various revenues and avoided costs that may be realized by installing a recovery scrubber similar in size to the one used at Dragon Products, simple payback on the investment is projected in as little as 3.1 years. In making this projection, $6,000,000 was added to the "as-built" capital costs to allow for contingency, design/permitting, construction interest, and licensing fees.

Commercial Applications

Of the approximately 2,000 Portland cement kilns in the world, about 250 are in the United States and Canada. These 250 kilns emit an estimated 230,000 tons/yr of SO_2 (only three plants have SO_2 controls, one of which is the Passamaquoddy Technology Recovery Scrubber™). The applicable market for SO_2 control is estimated at 75% of the 250 installations. If full penetration of this estimated market were realized, approximately 150,000 tons/yr of SO_2 reduction could be achieved.

The scrubber became a permanent part of the cement plant at the end of the demonstration. A feasibility study has been completed for a Taiwanese cement plant.

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References

- *Passamaquoddy Technology Recovery Scrubber™: Final Report.* Volumes 1 and 2 (Appendices A–M. Passamaquoddy Tribe. February 1994. (Vol. 1 available from NTIS as DE94011175, Vol. 2 as DE94011176.)
- *Passamaquoddy Technology Recovery Scrubber™: Public Design Report.* Report No. DOE/PC/89657-T2. Passamaquoddy Tribe. October 1993. (Available from NTIS as DE94008316.)
- *Passamaquoddy Technology Recovery Scrubber™: Topical Report.* Report No. DOE/PC/89657-T1. Passamaquoddy Tribe. March 1992. (Available from NTIS as DE92019868.)
- *Comprehensive Report to Congress on the Clean Coal Technology Program: Cement Kiln Flue Gas Recovery Scrubber.* (Passamaquoddy Tribe). Report No. DOE/FE-0152. U.S. Department of Energy. November 1989. (Available from NTIS as DE90004462.)

▲ The Passamaquoddy Technology Recovery Scrubber™ became a permanent part of the Dragon Products facility at the project's end.

Pulse Combustor Design Qualification Test

Participant
ThermoChem, Inc.

Additional Team Member
Manufacturing and Technology Conversion International, Inc. (MTCI)—technology supplier

Location
Baltimore, MD (MTCI Test Facility)

Technology
MTCI's PulsedEnhanced™ Steam Reforming using a multiple resonance tube pulse combustor.

Plant Capacity/Production
13 million Btu/hr (steam reformer)

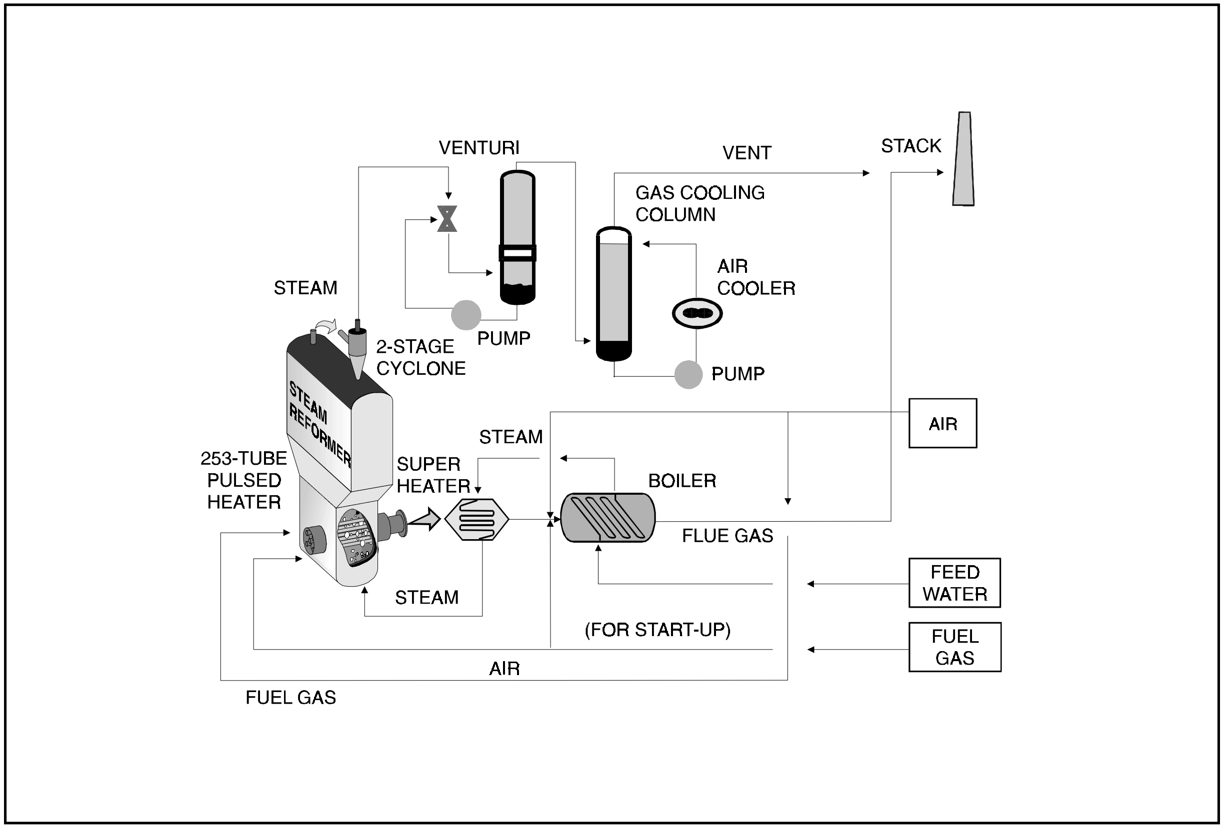
Coal
Powder River Basin subbituminous

Project Funding

Total project cost	$8,612,054	100%
DOE	4,306,027	50
Participants	4,306,027	50

Project Objective
To demonstrate the operational/commercial viability of a single 253-resonance-tube pulse combustor unit and evaluate characteristics of coal-derived fuel gas generated by an existing Process Development Unit.

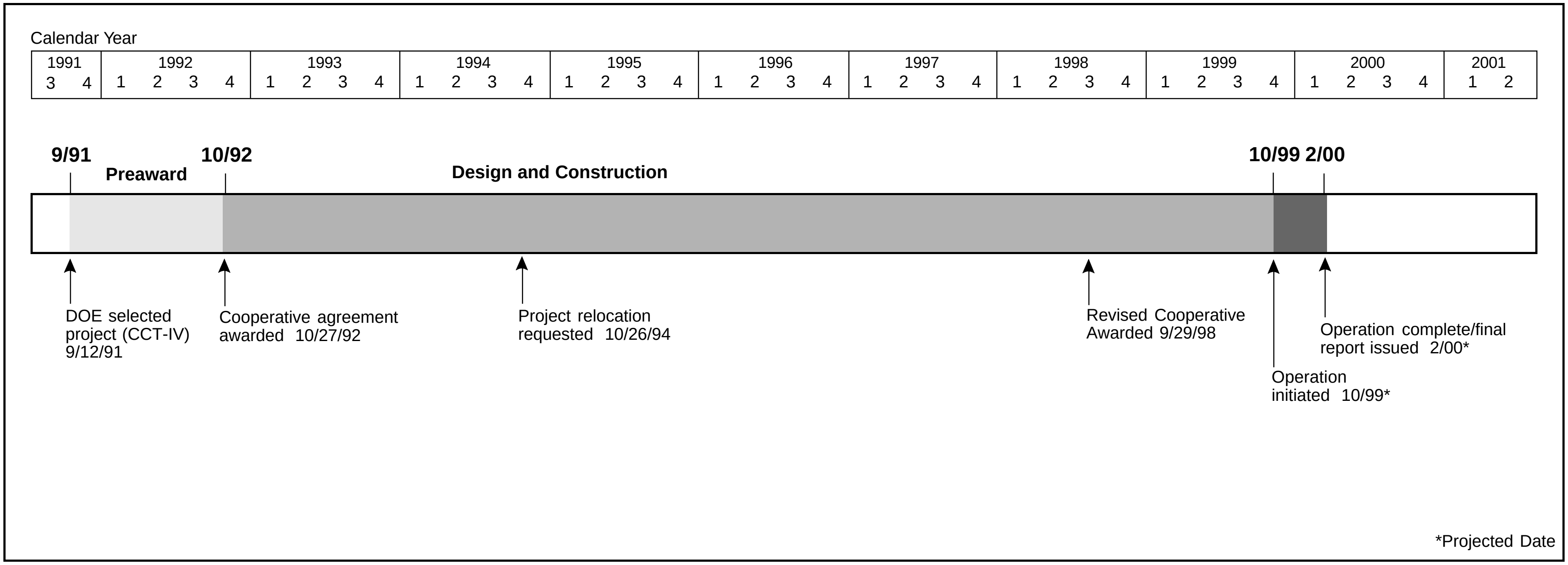
Technology/Project Description
MTCI's PulsedEnhanced™ Steam Reforming process incorporates an indirect heating process for thermochemical steam gasification of coal to produce hydrogen-rich, clean, medium-Btu content fuel gas without the need for an oxygen plant. Indirect heat transfer is provided by the multiple resonance-tube pulse combustor by immersing the combustor tubes in the fluidized-bed steam gasification reactor. Pulse combustion increases heat transfer rate by a factor of 3 to 5, thus greatly reducing the heat transfer area required in the gasifier.



The pulse combustor represents the core of the PulsedEnhanced™ Steam Reforming process because it provides a highly efficient and cost-effective heat source. Demonstration of the combustor at the 253-resonance-tube commercial scale is critical to market entry. The 253-resonance-tube unit represents a 3.5 scale-up from previous tests. Testing will seek to verify scale-up criteria and appropriateness of controls and instrumentation. Also, an existing Process Development Unit (PDU) will be used to gasify coal feedstock to provide fuel gas data, including energy content, species concentration, and yield. Char from the PDU will be evaluated as well.

The facility will also have a product gas cleanup train that includes two stages of cyclones, a venturi scrubber with a scrubber tank, and a gas quench column. An air-cooled heat exchanger will be used to reject heat from the condensation of excess steam (unreacted fluidization steam) quenched in the venturi scrubber and gas quench column. All project testing will be performed at the MTCI test facility in Baltimore, Maryland.

Project Status/Accomplishments
On September 10, 1998, DOE approved revision of ThermoChem, Inc.'s Cooperative Agreement for a scaled-down, 16-month project. The original project, awarded in October, 1992, was a commercial demonstration facility that would employ 10 identical 253-resonance-tube pulse combustor units. After fabrication of the first combustor unit, the project went through restructuring. The



revised project will demonstrate a single 253-resonance-tube pulse combustor. The first major milestone is completion of design by early 1999. NEPA requirements were satisfied on November 30, 1998 with a Categorical Exclusion.

Commercial Applications

PulsedEnhanced™ Steam Reforming has application in many different processes. Coal, with the world production on the order of four billion tons per year, constitutes the largest potential feed stock for steam reforming. Other potential feedstocks include spent liquor from pulp and paper mills, refused-derived fuel, municipal solid waste, sewage sludge, biomass, and other wastes.

Although the project will demonstrate mild gasification only, the following coal-based applications are envisioned:

- Coal processing for combined-cycle power generation,
- Coal processing for fuel cell power generation,
- Coal pond waste and coal rejects processing to produce a hydrogen-rich gas from the steam reformer for use in overfiring or reburning to reduce NO_x emissions,
- Coal processing for production of gas or liquid fuel and char for the steel industry,
- Coal processing for producing compliance fuels,
- Mild gasification of coal,
- Direct reduction steel production,
- Co-processing of coal and wastes, and
- Coal drying.

In addition, the technology has application for black liquor processing and chemical recovery and for hazardous, low-level radioactive, and low-level mixed waste volume reduction and destruction.

Appendix A: Historical Perspective and Legislative History

Historical Perspective

There were a number of key events that prompted creation of the CCT Program and impacted its focus over the course of the five solicitations. The roots of the CCT Program can be traced to the acid rain debates of the early 1980s, culminating in U.S. and Canadian envoys recommending a five year, $5 billion U.S. effort to curb precursors to acid rain formation—SO_2 and NO_x. This recommendation was adopted and became a presidential initiative in March 1987.

As a part of the response to the recommendations of the *Special Envoys on Acid Rain* in April 1987, the President directed the Secretary of Energy to establish a panel to advise the President on innovative clean coal technology activities. This panel was the Innovative Control Technology Advisory Panel. As a part of the panel's activities, the state and federal incentive subcommittee prepared a report, *Report to the Secretary of Energy Concerning Commercialization Incentives*, that addressed actions that states could take to provide incentives for demonstrating and deploying clean coal technologies. The panel determined that demonstration and deployment should be managed through both state and federal initiatives.

In the same time frame, the Vice President's Task Force on Regulatory Relief (later referred to as the Presidential Task Force on Regulatory Relief) was established. Among other things, the task force was asked to examine incentives and disincentives to the commercial realization of new clean coal technologies. The task force also examined cost-effective emissions reduction measures that might be inhibited by various federal, state, and local regulations. The task force recommended that preference be given to projects located in states that offer certain regulatory incentives to encourage such technologies. This recommendation was accepted and became part of the project selection considerations beginning with CCT-II.

Initial CCT Program emphasis was on controlling SO_2 and NO_x emissions from existing coal-based power generators. Approaches demonstrated through the program were coal processing to produce clean fuels, combustion modification to control emissions, postcombustion cleanup of flue gas, and repowering with advanced power generation systems. These early efforts (projects resulting from the first three solicitations) produced a suite of cost-effective compliance options available today to address acid rain concerns.

As the CCT Program evolved, work began on drafting what was to become the Clean Air Act Amendments of 1990. Through a dialog with EPA and Congress, the program was able to remain responsive to shifts in environmental emphasis. Also, projects in place enabled CAAA architects to have access to real-time data on emission control capabilities while structuring proposed acid rain regulations under Title IV of the CAAA. Aside from acid rain, there was an emerging issue in the area of hazardous air pollutants (HAPs), also referred to as air toxics. Title III of the CAAA listed 189 airborne compounds subject to control, including trace elements and volatile and semi-volatile compounds. To assess the impacts on coal-based power generation, CCT Program projects were leveraged to obtain data through an integrated effort among DOE, EPA, EPRI, and the Utility Air Regulatory Group. Through this effort, concerns about HAPs relative to coal-based power generation have been significantly mitigated, enabling focus on but a few flue gas constituents. Also, because NO_x is a precursor to ozone formation, the presence of NO_x in ozone nonattainment areas, even at low levels, became an issue. This precipitated action in the CCT Program to include technologies capable of deep NO_x reduction in the portfolio of technologies sought.

In the course of the last two solicitations of the CCT Program, a number of energy and environmental considerations combined to change the emphasis toward seeking high-efficiency, very-low-emission power generation technology. Energy demand projections in the United States showed the need for continued reliance on coal-based power generation, with significant growth required into the 21st century. The CAAA, however, capped SO_2 emissions at year 2000 levels, and NO_x continued to receive increased attention relative to ozone nonattainment. Furthermore, particulate emissions were coming under increased scrutiny because of correlations with lung disorders and the tendency for toxic compounds to adhere to particulate matter. Added to these concerns was the growing concern over global warming, and more specifically, the CO_2 produced from burning fossil fuels. Coal became a primary target because of the high carbon-to-hydrogen ratio relative to natural gas, resulting in somewhat higher CO_2 emissions per unit of energy produced. However, coal is the fuel of choice (if not necessity) for many developing countries where projected growth in electric power generation is the greatest. The path chosen to respond to these considerations was to pursue advanced power generation systems that could provide major enhancements in efficiency and control SO_2, NO_x, and particulates without introducing external parasitic control devices. (Increased efficiency translates to less coal consumption per unit of energy produced.) As a result, a number of advanced power generation projects were undertaken, representing pioneer efforts recognized throughout the world.

Legislative History

The legislation authorizing the CCT Program is found in Public Law 98-473, Joint Resolution Making Continuing Appropriations for Fiscal Year 1985 and for Other Purposes. Title I set aside $750 million of the congressionally rescinded $5.375 billion of the Synthetic Fuels Corporation into a special U.S. Treasury account entitled the "Clean Coal Technology Reserve." This account was dedicated to "conducting cost-shared clean coal technology projects for the construction and operation of facilities to demonstrate the feasibility of future commercial applications of such technology." Title III of this act directed the Secretary of Energy to solicit statements of interest in and proposals for clean coal projects. In keeping with this mandate, DOE issued a program announcement, which resulted in the receipt of 176 proposals representing both domestic and international projects with a total estimated cost in excess of $8 billion.

After this significant initial expression of interest in clean coal demonstration projects, Public Law 99-190, enacted December 1985, appropriated $400 million to conduct cost-shared demonstration projects. Of the total appropriated funds, approximately $387 million was made available for cost-shared projects to be selected through a competitive solicitation, or Program Opportunity Notice (PON), referred to as CCT-I. (The remaining funds were required for program direction and the legislatively mandated Small Business Innovation Research Program [SBIR] and Small Business Technology Transfer Program [STTR].)

In a manner similar to the initiation of CCT-I, Congress again directed DOE to solicit information from the private sector in the Department of the Interior and Related Agencies Appropriations Act for FY1987 (Public Law 99-591, enacted October 30, 1986). The information received was to be used to establish the level of potential industrial interest in another solicitation, this time involving clean coal technologies capable of retrofitting, repowering, or modernizing existing facilities. Projects were to be cost-shared, with industry sharing at least 50 percent of the cost. As a result of the solicitation, a total of 39 expressions of interest were received by DOE in January 1987.

On March 18, 1987, the President announced the endorsement of the recommendations of the Special Envoys on Acid Rain, including a $2.5 billion government share of funding for industry/government demonstrations of innovative control technology over a five year period. The Secretary of Energy stated that the department would ask Congress for an additional $350 million in FY1988 and an advanced appropriation of $500 million in FY1989. Additional appropriations of $500 million would be requested in fiscal years 1990, 1991, and 1992. This request was made by the President on April 4, 1987.

Public Law 100-202, enacted December 22, 1987, as amended by Public Law 100-446, appropriated a total of $575 million to conduct CCT-II. About $536 million was for projects, with the remainder for program direction and the SBIR and STTR Programs.

The Department of the Interior and Related Agencies Appropriations Act for FY1989 (Public Law 100-446, enacted September 27, 1988) provided $575 million for necessary expenses associated with clean coal technology demonstrations in the CCT-III solicitation. Of the total funding, about $546 million was made available for cost-sharing projects, with the remainder for program direction and the SBIR and STTR Programs. The act continued the requirement that proposals must demonstrate technologies capable of retrofitting or repowering existing facilities. The statute also authorized the use of Tennessee Valley Authority power program funds as a source of nonfederal cost-sharing, except if provided by annual appropriations acts. In addition, funds borrowed by Rural Electrification Administration)now Rural Utilities Service) electric cooperatives from the Federal Financing Bank became eligible as cost-sharing in the CCT-III solicitation, except if provided by annual appropriations.

In the Department of the Interior and Related Agencies Appropriations Act of 1990 (Public Law 101-121, enacted October 23, 1989), Congress provided $600 million for the CCT-IV solicitation. CCT-IV, according to the act, "shall demonstrate technologies capable of replacing, retrofitting, or repowering existing facilities and shall be subject to all provisos contained under this head in Public Laws 99-190, 100-202 and 100-446 as amended by this Act." About $563 million was made available for federal cofunding of projects selected in CCT-IV, with the remainder for program direction and the SBIR and STTR Programs.

In Public Law 101-121, enacted October 23, 1989, Congress also provided $600 million for the CCT-V solicitation. CCT-V, according to the act, "shall be subject to all provisos contained under this head in Public Laws 99-190, 100-202 and 100-446 as amended by this Act." Approximately $568 million was made available for federal cofunding of projects to be selected in this solicitation, with the remainder again for program direction and the SBIR and STTR Programs.

Subsequent acts (Public Laws 101-164, 101-302, 101-512, and 102-154) modified the schedule for issuing CCT-IV and/or CCT-V PONs and selecting projects. In Public Law 101-512, Congress directed DOE to issue the PON for CCT-IV not later than February 1, 1991, with selections to be made within 8 months. In Public Law 102-154, Congress directed DOE to issue CCT-V PON not later than July 6, 1992, with selections to be made within 10 months. This later act also directed that CCT-V proposals should advance significantly the efficiency and environmental performance of coal-using technologies and be applicable to either new or existing facilities.

Public Laws 101-164, 101-302, 101-512, 103-138, and 103-332 adjusted the rate at which funds were to be made available to the program.

CCT Program funds have been further adjusted through sequestering requirements of the Gramm-Rudman-Hollings Deficit Reduction Act as well as rescissions. Sequestering reduced CCT Program appropriations as follows:

- $2.4 million was sequestered from the $400 million appropriated by Public Law 99-190.
- $2,600 was sequestered from the $575 million appropriated by Public Law 100-202, as amended by Public Law 100-446.
- $2,028 was sequestered from the $575 million appropriated by Public Law 100-446, as amended by Public Law 101-164.
- $455 was sequestered from the $1.2 billion appropriated by Public Law 101-121, as amended by Public Laws 101-512, 102-154, 102-381, 103-138, 103-332, 104-6, 104-208, and 105-18.

Rescissions have reduced CCT Program appropriations as follows:

- $200 million was rescinded by Public Law 104-6.
- $123 million was rescinded by Public Law 104-208.
- $17 million was rescinded by Public Law 105-18.

In 1998, $40 million of the CCT program funds were deferred. Funds will be restored over a three year period beginning October 1, 1999.

Exhibit A-1 lists all the key legislation relating to the CCT Program and provides a summary of provisions relating to program funding as well as program implementation. Following this exhibit are funding provisions excerpted from appropriations and other relevant funding-related acts.

Exhibit A-1
CCT Program Legislative History

Public Law	Date Enacted	CCT Round	Program Funding	Implementation Provisions
98-473	10/12/84	Initiation of CCT Program; informational solicitation	Rescinded $750 million of $5.375 billion from the Energy Security Reserve (Synthetic Fuels Corporation) to be deposited in a U.S. Treasury Department account entitled “Clean Coal Technology Reserve” for conducting cost-shared CCT projects for the construction and operation of facilities to demonstrate the feasibility for future commercial application of such technology, without fiscal year limitation, subject to subsequent annual appropriation.	Title III required publication of a notice soliciting statements of interest in and proposals for projects employing emerging CCTs. A report to Congress was required no later than 4/15/85.
99-88	8/15/85		Deferred $1.6 million for obligation until 10/1/85.	Conference Report (H. Rep. 99-236) concurred with CCT project guidelines contained in Senate Report 99-82, with certain modifications.
99-190	12/19/85	CCT-I	Conference Report (H. Rep. 99-450) agreed to a $400-million CCT Program as described under the U.S. Treasury Department Energy Security Reserve, with the request for proposals to be for the full $400 million.	Required a PON (CCT-I) to be issued and projects to be selected no later than 8/1/86. Project cost-sharing provisions were detailed.
99-591	10/30/86	Second informational solicitation	(Contained no funding provisions for CCT Program)	Title II required publication of a notice soliciting statements of interest in, and informational proposals for projects employing emerging CCTs capable of retrofitting, repowering, or modernizing existing facilities. A report to Congress was required no later than 3/6/87.
100-202	12/22/87	CCT-II	Appropriated $50 million for FY beginning 10/1/87 until expended and $525 million for FY beginning 10/1/88 until expended.	Required a request for proposals (CCT-II) to be issued no later than 60 days following enactment, for emerging CCTs capable of retrofitting or repowering existing facilities. Extended project selection from 120 days to 160 days after receipt of proposals. Provided for cost-sharing of pre-award costs for preparation and submission of environmental data upon signing of the cooperative agreement. Conference Report (H. Rep. 100-498) provided that project cost-sharing funds be made available to nonutility as well as utility applications. No funds were made available for new, stand-alone applications. H. Rep. Report 100-171 and Senate Report 100-165 outlined provisions for participant to repay government contributions.

Exhibit A-1 (continued)
CCT Program Legislative History

Public Law	Date Enacted	CCT Round	Program Funding	Implementation Provisions
100-446	9/27/88	CCT-III	Made available $575 million on 10/1/89 until expended. Pub. L. 100-202 was amended by striking $525 million and inserting $190 million for FY beginning 10/1/88 until expended, $135 million for fiscal year beginning 10/1/89 until expended, and $200 million for FY beginning 10/1/90 until expended, provided that outlays for FY89 resulting from use of funds appropriated under Pub. L. 100-202, as amended, did not exceed $15.5 million.	Request for proposals (CCT-III) to be issued by 5/1/89 for emerging CCTs capable of retrofitting or repowering existing facilities. Proposals were to be due 120 days after issuance of the PON; projects were to be selected no later than 120 days after receipt of proposals. Funds borrowed by REA electric cooperatives from the Federal Financing Bank were made eligible as cost-sharing. Funds derived by the Tennessee Valley Authority from its power program were deemed allowable as cost-sharing except if provided by annual appropriations acts.
101-45	6/30/89	CCT-III	Funds appropriated for FY1989 were made available for a third solicitation.	Project selections for the third solicitation were to be made not later than 1/1/90.
101-121	10/23/89	CCT-IV and CCT-V	Made available $600 million on 10/1/90 until expended and $600 million on 10/1/91 until expended. Pub. L. 100-446 was amended by striking $575 million and inserting $450 million to be made available on 10/1/89 until expended and $125 million to be made available on 10/1/90. Unobligated balances excess to the needs of the procurement for which they originally were made available may be applied to other procurements for which requests for proposals had not yet been issued, except that no supplemental, backup, or contingent selection of projects could be made over and above the projects originally selected.	Two solicitations (CCT-IV and CCT-V) to be issued, one for each appropriation, to demonstrate technologies capable of replacing, retrofitting, or repowering existing facilities, subject to all provisos contained in Pub. L. 99-190, 100-202, and 100-446 as amended. The PON (CCT-IV) using funds becoming available on 10/1/90 was to be issued by 6/1/90, with selections made by 2/1/91. The PON (CCT-V) using funds becoming available on 10/1/91 was to be issued no later than 9/1/91, with selections made by 5/1/92.
101-164	11/21/89	CCT-IV and CCT-V	Appropriation for FY1990 was amended by striking $450 million and inserting $419 million and by striking $125 million and inserting $156 million.	
101-302	5/25/90	CCT-IV and CCT-V	Obligation of funds previously appropriated for CCT-IV and CCT-V was deferred until 9/1/91.	Solicitations could not be conducted prior to ability to obligate funds. Repayment provisions for CCT-IV and CCT-V were to be the same as for CCT-III.

Exhibit A-1 (continued)
CCT Program Legislative History

Public Law	Date Enacted	CCT Round	Program Funding	Implementation Provisions
101-512	11/5/90	CCT-IV and CCT-V	Pub. L. 101-121 was amended by striking $600 million made available on 10/1/90 until expended and $600 million made available on 10/1/91 until expended and inserting $600 million made available as follows: $35 million on 9/1/91, $315 million on 10/1/91, and $250 million on 10/1/92, all sums remaining until expended, for use in conjunction with a separate general request for proposals, and $600 million made available as follows: $150 million on 10/1/91, $225 million on 10/1/92, and $225 million on 10/1/93, all sums remaining until expended, for use with a separate general request for proposals.	The CCT-IV solicitation was to be issued not later than 2/1/91. The CCT-V PON was to be issued not later than 3/1/92. Project selections were to be made within eight months of PON's issuance. Repayment provisions were to be the same as for CCT-III. Provisions were included to provide protections for trade secrets and proprietary information. Conference Report (H. Rep. 101-971) recommends changes to program policy factors.
102-154	11/13/91	CCT-V	Pub. L. 102-512 was amended by striking $150 million on 10/1/91 and $225 million on 10/1/92 and inserting $100 million on 10/1/91 and $275 million on 10/1/92.	The CCT-V PON was delayed to not later than 7/6/92, with selection to be made within 10 months (extended by two months). The PON was to be for projects that advance significantly the efficiency and environmental performance of coal-using technologies and be applicable to either new or existing facilities. Conference Report (H. Rep. 102-256) stated expectations that the CCT-V solicitation would be conducted under the same general types of criteria as CCT-IV, principally modified only to (1) include the wider range of eligible technologies or applications; (2) adjust technical criteria to consider allowable development activities, strengthen criteria for nonutility demonstrations, and adjust commercial performance criteria for additional facilities and technologies with regard to aspects of general energy efficiency and environmental performance; and (3) clarify and strengthen cost and finance criteria, particularly with regard to development activities. Funding was allowed for project-specific development activities for process performance definition, component design verification, materials selection, and evaluation of alternative designs on a cost-shared basis up to a limit of 10 percent of the government share of project cost.

Exhibit A-1 (continued)
CCT Program Legislative History

Public Law	Date Enacted	CCT Round	Program Funding	Implementation Provisions
102-154 (continued)				Development activities eligible for cost-sharing included limited modifications to existing facilities for project-related testing but not construction of new facilities.
102-381	10/5/92		Pub. L. 101-512 was amended by striking $250 million on 10/1/92 and inserting $150 million on 10/1/93 and $100 million on 10/1/94; and by striking $275 million on 10/1/92 and $225 million on 10/1/93 and inserting $250 million on 10/1/93 and $250 million on 10/1/94.	
102-486	10/24/92		(Contained no funding provisions for CCT Program)	Section 1301—Coal RD&D and Commercial Applications Programs (Title XIII; Subtitle A) authorized DOE to conduct programs for RD&D and commercial applications of coal-based technologies. Secretary of Energy was directed to submit to Congress (1) a report that included, among other things, recommendations regarding the manner in which the cost-sharing demonstrations conducted pursuant to the Clean Coal Program (Pub. L. 98-473) might be modified and extended in order to ensure the timely demonstration of advanced coal-based technologies and (2) periodic status reports on the development of advanced coal-based technologies and RD&D and commercial application attributes.
103-138	11/11/93		Pub. L. 101-512 was amended by striking $150 million on 10/1/93 and $100 million on 10/1/94 and inserting $100 million on 10/1/93, $100 million on 10/1/94, and $50 million on 10/1/95; and by striking $250 million on 10/1/93 and $250 million on 10/1/94 and inserting $125 million on 10/1/93, $275 million on 10/1/94, and $100 million on 10/1/95.	
103-332	9/30/94		Pub. L. 101-512 was amended by striking $100 million on 10/1/94 and $50 million on 10/1/95 and inserting $18 million on 10/1/94, $100 million on 10/1/95, and $32 million on 10/1/96; and by striking $275 million on 10/1/94 and $100 million on 10/1/95 and inserting $19.121 million on 10/1/94, $100 million on 10/1/95, and $255.879 million on 10/1/96.	An amount not to exceed $18 million available in FY1995 may be used for administrative oversight of the CCT Program.

Exhibit A-1 (continued)
CCT Program Legislative History

Public Law	Date Enacted	CCT Round	Program Funding	Implementation Provisions
104-6	4/10/95		Of funds available for obligation in FY1996, $50 million was rescinded. Of the funds to be made available for obligation in FY1997, $150 million was rescinded.	
104-134[a]	4/26/96			Conference Report (H. Rep. 104-402 to accompany H.R. 1977) allowed for the use of up to $18 million in CCT Program funds for program administration.
104-208[b]	9/30/96		Conference Report (H. Rep. 104-863 to accompany H.R. 3610) noted rescission of $123 million for FY1997 or prior years.	House and Senate committees did not object to use of up to $16 million in available funds for administration of the CCT Program in FY1997 (H. Rep. 104-625 and Senate 104-319 to accompany H.R. 3662).
105-18	6/12/97		Of funds made available for obligation in FY1997 or prior years, $17 million was rescinded.	
105-83	11/14/97		Of funds made available for obligation in FY1997 or priors, $101 million was rescinded.	
105-277	10/21/98		Of funds made available for obligation in prior years, $40 million was deferred.	Conference Report allowed $14.9 million in CCT Program funds for program administration.

[a] H.R. 3019, which became Pub. L. 104-134, replaced H.R. 1977.

[b] H.R. 3610, which became Pub. L. 104-208, replaced H.R. 3662.

Public Law 99-190

Public Law 99-190, 99 Stat. 1251 (1985)

Clean Coal Technology

Within 60 days following enactment of this Act [Dec. 19, 1985] the Secretary of Energy shall, pursuant to the Federal Nonnuclear Energy Research and Development Act of 1974 *(42 U.S.C. 5901*, et seq.), issue a general request for proposals for clean coal technology projects for which the Secretary of Energy upon review may provide financial assistance awards. Proposals for clean coal technology projects under this section shall be submitted to the Department of Energy within 60 days after issuance of the general request for proposals. The Secretary of Energy shall make any project selections no later than August 1, 1986: Provided, That the Secretary may vest fee title or other property interests acquired under cost-shared clean coal technology agreements in any entity, including the United States: Provided further, That the Secretary shall not finance more than 50 per centum of the total costs of a project as estimated by the Secretary as of the date of award of financial assistance: Provided further, That cost-sharing by project sponsors is required in each of the design, construction, and operating phases proposed to be included in a project: Provided further, That financial assistance for costs in excess of those estimated as of the date of award of original financial assistance may not be provided in excess of the proportion of costs borne by the Government in the original agreement and only up to 25 per centum of the original financial assistance: Provided further, That revenues or royalties from prospective operation of projects beyond the time considered in the award of financial assistance, or proceeds from prospective sale of the assets of the project, or revenues or royalties from replication of technology in future projects or plants are not cost-sharing for the purposes of this appropriation: Provided further, That other appropriated Federal funds are not cost-sharing for the purposes of this appropriation: Provided further, That existing facilities, equipment, and supplies, or previously expended research or development funds are not cost-sharing for the purposes of this appropriation, except as amortized, depreciated, or expensed in normal business practice.

Conference Report (H.R. Conf. Rep. No. 450, 99th Cong., 1st Sess. [1985])

Clean Coal Technology

The managers have agreed to a $400,000,000 Clean Coal Technology program as described under the Department of the Treasury, Energy Security Reserve. Bill language is included which provides for the selection of projects no later than August 1, 1986. Within that period, a general request for proposals must be issued within 60 days and proposals must be submitted to the Department within 60 days after issuance of the general request for proposals. Language is also included allowing the Secretary of Energy to vest title in interests acquired under agreements in any entity, including the United States, and delineating cost-sharing requirements. Funds for these activities and projects are made available to the Clean Coal Technology program in the Energy Security program.

It is the intent of the managers that contributions in the form of facilities and equipment be considered only to the extent that they would be amortized, depreciated or expensed in normal business practice. Normal business practice shall be determined by the Secretary and is not necessarily the practice of any single proposer. Property which has been fully depreciated would not receive nay cost-sharing value except to the extent that it has been in continuous use by the proposer during the calendar year immediately preceding the enactment of this Act. For this property, a fair use value for the life of the project may be assigned. Property offered as a cost-share by the proposer that is currently being depreciated would be limited in its cost-share value to the depreciation claimed during the life of the demonstration project. Furthermore, in determining normal business practice, the Secretary should not accept valuation for property sold, transferred, exchanged, or otherwise manipulated to acquire a new basis for depreciation purposes or to establish a rental value in circumstances which would amount to a transaction for the mere purpose of participating in this program.

The managers agree that, with respect to cost-sharing, tax implications of proposals and tax advantages available to individual proposers should not be considered in determining the percentage of Federal cost-sharing. This is consistent with current and historical practices in Department of Energy procurements.

It is the intent of the managers that there be full and open competition and that the solicitation be open to all markets utilizing the entire coal resource base. However, projects should be limited to the use of United States mined coal as the feedstock and demonstration sites should be located within the United States.

The managers agree that no more than $1,500,000 shall be available in FY1986 and $2,000,000 each year thereafter for contracting, travel and ancillary costs of the program, and that manpower costs are to be funded under the fossil energy research and development program.

The managers direct the Department, after projects are selected, to provide a comprehensive report to the Congress on proposals received.

The managers also expect the request for proposals to be or the full $400,000,000 program, and not only for the first $100,000,000 available in fiscal year 1986.

Public Law 100-202

Public Law 100-202, 101 Stat. 1329-1 (1987)

Clean Coal Technology

For necessary expenses of, and associated with, Clean Coal Technology demonstrations pursuant to 42 U.S.C. 5901 et seq., $50,000,000 are appropriated for the fiscal year beginning October 1, 1987, and shall remain available until expended, and $525,000,000 are appropriated for the fiscal year beginning October 1, 1988, and shall remain available until expended.

No later than sixty days following enactment of this Act, the Secretary of Energy shall, pursuant to the Federal Nonnuclear Energy Research and Development Act of 1974 (42 U.S.C. 5901 et seq.), issue a general request for proposals for emerging clean coal technologies which are capable of retrofitting or repowering existing facilities, for which the Secretary of Energy upon review may provide financial assistance awards. Proposals under this section shall be submitted to the Department of Energy no later than ninety days after issuance of the general request for proposals required herein, and the Secretary of Energy shall make any project selections no later than one hundred and sixty days after receipt of proposal: *Provided*, That projects selected are subject to all provisos contained under this head in Public Law 99-190: *Provided further*, That pre-award costs incurred by project sponsors after selection and before signing an agreement are allowable to the extent that they are related to (1) the preparation of material requested by the Department of Energy and identified as required for the negotiation; or (2) the preparation and submission of environmental data requested by the Department of Energy to complete National Environmental Policy Act requirements for the projects: *Provided further*, That pre-award costs are to be reimbursed only upon signing of the project agreement and only in the same ratio as the cost-sharing for the total project: *Provided further*, That reports on projects selected by the Secretary of Energy pursuant to authority granted under the heading "Clean coal technology" in the Department of the Interior and Related Agencies Appropriations Act, 1986, as contained in Public Law 99-190, which are received by the Speaker of the House of Representatives and the President of the Senate prior to the end of the first session of the 100th Congress shall be deemed to have met the criteria in the third proviso of the fourth paragraph under the heading "Administrative provision, Department of Energy" in the Department of the Interior and Related Agencies Appropriations Act, 1986, as contained in Public Law 99-190, upon expiration of 30 calendar days from receipt of the report by the Speaker of the House of Representatives and the President of the Senate.

Conference Report (H.R. Conf. Rep. No. 498, 100th Cong., 1st Sess. [1987])

Clean Coal Technology

Appropriates $575,000,000 for clean coal technology instead of $350,000,000 as proposed by the House and $850,000,000 as proposed by the Senate. The comparison by year is as follows:

	House	Senate	Conference
Fiscal year:			
1988	$50,000,000	$350,000,000	$50,000,000
1989	200,000,000	500,000,000	525,000,000
1990	100,000,000	—	—
Total	**350,000,000**	**850,000,000**	**575,000,000**

Bill language, proposed by the House, which would have prohibited using grants has been deleted. The managers agree that project funding is expected to be based on cooperative agreements, but that grants might be applicable to support work also funded from this account.

The managers agree to deleted Senate language providing personnel floors for Clean Coal Technology. The managers further agree that the budget estimates for personnel and contract support are to be followed. The agreement included 58 new positions above current employment floors for the fossil energy organization and 30 positions within the floors. Out of clean coal technology funds, up to $3,980,000 is for fiscal year 1988 personnel-related costs and up to $16,520,000 is for all contract costs needed to make project selections and complete negotiations for both clean coal procurements. Contract costs necessary to monitor approved projects should be requested in the fiscal year 1989 budget. Increases above to those amount are subject to reprogramming procedures. No funds other than personnel related costs for the 30 positions included in the program direction are to be provided from the fossil energy research and development account.

The length of time for selection of projects by the Secretary of Energy has been extended from 120 days to 160 days based on experience from the original clean coal procurement. Once projects have been selected the Secretary should establish project milestones and guidelines for project negotiations in order to expedite the negotiation process to the extent feasible.

The managers agree that the funds provided are available for non-utility applications as well as for utility applications.

The managers agree that no funds are provided for the demonstration of clean coal technologies which are intended solely for new, stand alone, applications. The Senate had proposed up to 25% of the funds be available for this purpose.

Bill language has been included which provides that reports on projects selected in the first round of clean coal procurements that are received before the end of the first session of the 100th Congress will satisfy reporting requirements 30 calendar days after receipt by Congress. This provision applies to a maximum of two project reports.

Public Law 100-446

Public Law 100-446, 102 Stat. 1774 (1988)

Clean Coal Technology

For necessary expenses of, and associated with, Clean Coal Technology demonstrations pursuant to 42 U.S.C. 5901 et seq., $575,000,000 shall be made available on October 1, 1989, and shall remain available until expended: *Provided*, That projects selected pursuant to a general request for proposals issued pursuant to this appropriation shall demonstrate technologies capable of retrofitting or repowering existing facilities and shall be subject to all provisions contained under this head in Public Laws 99-190 and 100-202 as amended by this Act.

The first paragraph under this head in Public Law 100-202 is amended by striking “and $525,000,000 are appropriated for the fiscal year beginning October 1, 1988” and inserting “$190,000,000 are appropriated for the fiscal year beginning October 1, 1988, and shall remain available until expended, $135,000,000 are appropriated for the fiscal year beginning October 1, 1989, and shall remain available until expended, and $200,000,000 are appropriated for the fiscal year beginning October 1, 1990”: *Provided*, That outlays in fiscal year 1989 resulting from the use of funds appropriated under this head in Public Law 100-202, as amended by this Act, may not exceed $15,500,000: *Provided further*, That these actions are taken pursuant to section 202(b)(1) of Public law 100-119 (2 U.S.C. 909).

For the purposes of the sixth proviso under this head in Public Laws 99-190, funds derived by the Tennessee Valley Authority from its power program are hereafter not to be precluded from qualifying as all or part of any cost-sharing requirement, except to the extent that such funds are provided by annual appropriations Acts: *Provided*, That unexpended balances of funds made available in the “Energy Security Reserve” account in the Treasury for the Clean Coal Technology Program by the Department of the Interior and Related Agencies Appropriations Acts, 1986, as contained in section 101(d) of Public Law 99-190, shall be merged with this account: *Provided further*, That for the purposes of the sixth proviso in Public Law 99-190 under this heading, funds provided under section 306 of Public Law 93-32 shall be considered non-Federal: *Provided further*, That reports on projects selected by the Secretary of Energy pursuant to authority granted under the heading “Clean coal technology” in the

Department of the Interior and Related Agencies Appropriations Act, 1986, as contained in Public Law 99-190, which are received by the Speaker of the House of Representatives and the President of the Senate prior to the end of the second session of the 100th Congress shall be deemed to have met the criteria in the third proviso of the fourth paragraph under the heading "Administrative provisions, Department Energy" in the Department of the Interior and Related Agencies Appropriations Act, 1986, as contained in Public Law 99-190, upon expiration of 30 calendar days from receipt of the report by the Speaker of the House of Representatives and the President of the Senate.

Conference Report (H.R. Conf. Rep. No. 862, 100th Cong., 2nd Sess. [1988])

Clean Coal Technology

Amendment No. 131: Reported in technical disagreement. The managers on the part of the House will offer a motion to recede and concur in the amendment of the Senate with an amendment as follows:

In lieu of the matter proposed by said amendment insert the following: *For necessary expenses of, and associated with, Clean Coal Technology demonstrations pursuant to 42 U.S.C. 5901 et seq., $575,000,000 shall be made available on October 1, 1989, and shall remain available until expended: Provided, That projects selected pursuant to a general request for proposals issued pursuant to this appropriation shall demonstrate technologies capable of retrofitting or repowering existing facilities and shall be subject to all provisos contained under this head in Public Laws 99-190 and 100-202 as amended by this Act.*

The managers on the part of the Senate will move to concur in the amendment of the House to the amendment of the Senate. The amendment provides $575,000,000 in fiscal year 1990 for a third Clean Coal Technology procurement as proposed by the Senate, and clarifies that the procurement is for retrofit and repowering technologies and is subject to the cost-sharing provisions of the previous two procurements.

The managers agree that a request for proposals should be issued by May 1, 1989, with proposals due no later than 120 days after issuance of the request for proposals, and that the Secretary of Energy should make project selections no later than 120 days after receipt of proposals.

Amendment No. 132: Reported in technical disagreement. The managers on the part of the House will offer a motion to recede and concur in the amendment of the Senate with an amendment as follows:

Restore the matter stricken by said amendment, amended to read as follows: *The first paragraph under this head in Public Law 100-202 is amended by striking "and $525,000,000 are appropriated for the fiscal year beginning October 1, 1988" and inserting "$190,000,000 are appropriated for the fiscal year beginning October 1, 1988, and shall remain available until expended, $135,000,000 are appropriated for the fiscal year beginning October 1, 1989, and shall remain available until expended, and $200,000,000 are appropriated for the fiscal year beginning October 1, 1990": Provided, That outlays in fiscal year 1989 resulting from the use of funds appropriated under this head in Public Law 100-202, as amended by this Act, may not exceed $15,500,000: Provided further, That these actions are taken pursuant to section 202(b)(1) of Public Law 100-119 (2 U.S.C. 909).*

The managers on the part of the Senate will move to concur in the amendment of the House to the amendment of the Senate. The amendment changes the availability of $525,000,000 originally made available for fiscal year 1989 in Public Law 100-202 by making $190,000,000 available in 1989, $135,000,000 available in 1990, and $200,000,000 available in 1991 and also provides an outlay ceiling in fiscal year 1989. The House had proposed $100,000,000 in fiscal year 1989, $225,000,000 in fiscal year 1990, and $200,000,000 in fiscal year 1989, $225,000,000 in fiscal year 1990, and $200,000,000 in fiscal year 1991, and the Senate struck the House language.

Both of these changes are necessary because of budget allocation constraints, but neither action has an effect on the execution of the Clean Coal program, or on the Congress' overall support for the program, as is evidenced by additional appropriations provided for a third procurement of technologies.

The managers agree that administrative contract expenses may be incurred up to the budget level of $9,820,000, but caution that close control of such expenditures is necessary to assure that the outlay ceiling provided will be sufficient to cover project costs.

Amendment No. 133: Modifies public law citation as proposed by the Senate.

Amendment No. 134: Reported in technical disagreement. The managers on the part of the House will offer a motion to recede and concur in the amendment of the Senate which clarifies that funds borrowed by REA Electric Cooperatives from the Federal Financing Bank are eligible as cost-sharing in the clean coal technology program.

Amendment No. 135: Reported in technical disagreement. The managers on the part of the House will offer a motion to recede and concur in the amendment of the Senate which specifies clean coal projects may proceed 30 calendar days after receipt by Congress of required reports, provided the reports are received prior to the end of the 100th Congress.

Public Law 101-45

Public Law 101-45, 103 Stat. 97 (1989)

CLEAN COAL TECHNOLOGY

Notwithstanding any other provision of law, funds originally appropriated under this head in the Department of the Interior and Related Agencies Appropriations Act, 1989, shall be available for a third solicitation of clean coal technology demonstration projects, which projects are to be selected by the Department not later than January 1, 1990.

Public Law 101-121

Public Law 101-121, 103 Stat. 701 (1989)

CLEAN COAL TECHNOLOGY

For necessary expenses of, and associated with, Clean Coal Technology demonstrations pursuant to 42 U.S.C. 5901 et seq., $600,000,000 shall be made available on October 1, 1990, and shall remain available until expended, and $600,000,000 shall be made available on October 1, 1991, and shall remain available until expended: Provided, That projects selected pursuant to a separate general request for proposals issued pursuant to each of these appropriations shall demonstrate technologies capable of replacing, retrofitting or repowering existing facilities and shall be subject to all provisos contained under this head in Public Laws 99-190, 100-202, and 100-446 as amended by this Act: Provided further, That the general request for proposals using funds becoming available on October 1, 1990, under this paragraph shall be issued no later than June 1, 1990, and projects resulting from such a solicitation must be selected no later than February 1, 1991: Provided further, That the general request for proposals using funds becoming available on October 1, 1991, under this paragraph shall be issued no later than September 1, 1991, and projects resulting from such a solicitation must be selected no later than May 1, 1992.

The first paragraph under this head in Public Law 100-446 is amended by striking "$575,000,000 shall be made available on October 1, 1989" and inserting "$450,000,000 shall be made available on October 1, 1989, and shall remain available until expended, and $125,000,000 shall be made available on October 1, 1990": Provided, That these actions are taken pursuant to section 202(b)(1) of Public Law 100-119 (2 U.S.C. 909).

With regard to funds made available under this head in this and previous appropriations Acts, unobligated balances excess to the needs of the procurement for which they originally were made available may be applied to other procurements for which requests for proposals have not yet been issued: Provided, That for all procurements for which project selections have not been made as of the date of enactment of this Act no supplemental, backup, or contingent selection of projects shall be made over and above projects originally selected for negotiation and utilization of available funds: Provided further, That reports on projects selected by the Secretary of Energy pursuant to authority granted under this heading which are received by the Speaker of the House of Representatives and the President of the Senate less than 30 legislative days prior to the end of the first session of the 101st Congress shall be deemed to have met the criteria in the third proviso of the fourth paragraph under the heading "Administrative provisions, Department of Energy" in the Department of the Interior and Related Agencies Appropriations Act, 1986, as contained in Public Law 99-190, upon expiration of 30 calendar days from receipt of the report by the Speaker of the House of Representatives and the President of the Senate or at the end of the session, whichever occurs later.

Conference Report (H.R. Conf. Rep. No. 264, 101st Cong., 1st Sess. [1987])

Clean Coal Technology

Amendment No. 112: Reported in technical disagreement. The managers on the part of the House will offer a motion to recede and concur in the amendment of he Senate which adds the word "replacing" to the definition of clean coal technology. The managers agree that the inclusion of "replacing" for clean coal IV and V is intended to cover the complete replacement of an existing facility if because of design or site specific limitations, repowering or retrofitting of the plant is not a desirable option.

Amendment No,. 113: Appropriates $450,000,000 for fiscal year 1990 for clean coal technology instead of $500,000,000 as proposed by the House and $325,000,000 as proposed by he Senate. This appropriation along with $125,000,000 provided for fiscal year 1991 in Amendment 114 fully funds the third round of clean coal technology projects. The managers agree that additional manpower is required, particularly at the Department's Energy Technology Centers, in order to manage adequately the increased workload from the accumulation of active clean coal technology projects and the inclusion of additional procurements in this bill. Although a legislative floor is not included, the managers agree that at least eighty personnel will be required in addition to the approximately thirty FTE's now included in the fossil energy research and development appropriation. The managers agree further that funds from the fossil energy research and development appropriation should not be used to pay the cost of more than the equivalent FTE's paid under that account in fiscal year 1989.

Amendment No. 114: Reported in technical disagreement. The managers on the part of the House will offer a motion to recede and concur in the amendment of the Senate with an amendment as follows:

In lieu of the matter stricken and inserted by said amendment, insert: *and shall remain available until expended, and $125,0000,000*

The managers on the part of the Senate will move to concur in the amendment of the House to the amendment of the Senate. The amendment provides $125,000,000 in fiscal year 1991 for the third clean coal technology procurement instead of $75,000,000 as proposed by the House and $100,000,000 as proposed by the Senate.

Amendment No 115: Deletes Senate proposed appropriation of $150,000,000 for fiscal year 1992 for clean coal technology. The House proposed no such appropriation.

Amendment No. 116: Restores House language stricken by the Senate which prohibits the use of supplemental, backup, or contingent project selections in clean coal technology procurements.

Amendment No. 117: Restores the word "further" stricken by the Senate.

Public Law 101-164

Public Law 101-164, 103 Stat. 1069 (1989)

Clean Coal Technology

The second paragraph under this head contained in the Act making appropriations for the Department of the Interior and Related Agencies for the fiscal year ending September 30, 1990, is amended by striking "$450,000,000" and inserting "$419,000,000" and by striking "$125,000,000" and inserting "$156,000,000".

Conference Report (H.R. Conf. Rep. No. 315, 101st Cong., 1st Sess. [1989])

The managers have agreed to reduce the funds appropriated by the Energy and Water Development Appropriations Act for Fiscal Year 1990 (Public Law 101-101) for the "Nuclear Waste Disposal Fund" by $46,000,000. This reduction will make funds available for the drug prevention effort.

The managers have agreed to reductions to the Interior and Related Agencies Appropriations Act for Fiscal Year 1990 (Public Law 101-121) in order to accommodate additional drug related appropriations.

The reductions are in three areas. The new budget authority for Clean Coal Technology of $450,000,000 for fiscal year 1990 is reduced by $31,000,000 with this same amount added to the advance appropriation for fiscal year 1991. With this change the new amount for fiscal year 1990 is $419,000,000 while fiscal year 1991 increases to $156,000,000. The second area of change is the imposition of an outlay ceiling on Strategic Petroleum Reserve oil acquisition. Outlays will be reduced from an estimated $169,945,000 to $147,125,000 and will decrease the fill rate from approximately 50,000 barrels per day to approximately 46,000 or 47,000 barrels per day. The third reduction relates to the Pennsylvania Avenue Development Corporation. The borrowing authority is reduced from $5,000,000 to $100,000.

The conference agreement includes bill language reducing the amount of funds transferred from trust funds to the Health Care Financing Administration Program Management account by $32,000,000 from $1,917,172,000 to $18,851,712,000. This reduction, along with the outlays reserved from the regular 1990 Labor, Health and Human Services, and Education appropriations bill, will be sufficient to support the Subcommittee's share of the cost of anti-drug abuse funding. The conferees intend that the reduction in trust fund transfers be associated with activities to implement catastrophic health insurance, where funding needs may be diminished.

Public Law 101-302

Public Law 101-302, 104 Stat. 213 (1990)

Clean Coal Technology

Funds previously appropriated under this head for clean coal technology solicitations to be issued no later than June 1, 1990, and no later than September 1, 1991, respectively, shall not be obligated until September 1, 1991: Provided, That the aforementioned solicitations shall not be conducted prior to the ability to obligate these funds: Provided further, That pursuant to section 202(b) of the Balanced Budget and Emergency Deficit Control Reaffirmation Act of 1987, this action is a necessary (but secondary) result of a significant policy change: Provided further, That for the clean coal solicitations identified herein, provisions included for the repayment of government contributions to individual projects shall be identical to those included in the Program Opportunity Notice (PON) for Clean Coal Technology III (CCT-III) Demonstration Projects (solicitation number DE-PSO1-89 FE 61825), issued by the Department of Energy on May 1, 1989.

Conference Report (H.R. Conf. Rep. No. 493, 101st Cong., 2nd Sess. [1990])

Clean Coal Technology

Amendment No. 89. Reported in technical disagreement. The managers on the part of the House will offer a motion to recede and concur in the amendment of the senate with an amendment as follows:

In lieu of the matter proposed by said amendment insert:

Department of Energy
Clean Coal Technology

Funds previously appropriated under this head for clean coal technology solicitations to be issued no later than June 1, 1990, and no later than September 1, 1991, respectively, shall not be obligated until September 1, 1991: Provided, That the aforementioned solicitations shall not be conducted prior to the ability to obligate these funds: Provided further, That pursuant to section 202 (b) of the Balanced Budget and Emergency Deficit Control reaffirmation /Act of 1987 this action is a necessary (but secondary) result of a significant policy change: Provided further, That for the clean coal solicitations identified herein, provisions included for the repayment of government contributions to individual projects shall be identical to those included in the Program Opportunity Notice (PON) for Clean Coal Technology III (CCT-III) Demonstration Projects (solicitation number DE-PS01-89 FE 61825), issued by the Department of Energy on May 1, 1989.

The managers on the part of the Senate will move to concur in the amendment of the House to the amendment of the Senate.

The amendment delays the fourth and fifth clean coal technology solicitations as proposed by the Senate and specifies that, when issued, these solicitations must use repayment provisions used successfully in the third solicitation. This provision was included in the House introduced bill (H.R. 4828) and modifies a Senate amendment to the original Dire Emergency Supplemental.

The managers agree that changes to the clean air bill, proposed by a House authorizing committee, that would modify the clean coal technology program must be resolved before a reasonable solicitation can be issued. The proposed delay will allow such resolution.

The managers have added language to ensure that provisions dealing with the repayment of government provided funds will remain the same as the third round of procurements. These provisions were developed over a four year period based on experience of previous procurements and negotiations, and input from industrial participants, Congress, and the managers of the program. They appear to be working well.

Based on the long-term experience, and the clear fact that implementation of this type of technology will become even more important with passage of clean air legislation, the managers reject proposals put forth by the Department of Energy to increase rates substantially. Such proposals, while they might increase the recovery of government-provided funds over periods of up to 20 years, might also act as a deterrent to industrial participation in the program, which is already over 50 percent cost-shared by industry. The purpose of the program is to accelerate the introduction of clean uses of coal in a more efficient manner in compliance with stringent new air quality standards, not the provision of investment returns to the Government at the expense of nascent markets.

Public Law 101-512

Public Law 101-512, 104 Stat. 1915 (1990)

Clean Coal Technology

The first paragraph under this head in Public Law 101-121 is amended by striking "$600,000,000 shall be made available on October 1, 1990, and shall remain available until expended, and $600,000,000 shall be made available on October 1, 1991, and shall remain available until expended" and inserting "$600,000,000 shall be made available as follows: $35,000,000 on September 1, 1991, $315,000,000 on October 1, 1991, and $250,000,000 on October 1, 1992, all such sums to remain available until expended for use in conjunction with a separate general request for proposals, and $600,000,000 shall be made available as follows: $150,000,000 on October 1, 1991, $225,000,000 on October 1, 1992, and $225,000,000 on October 1, 1993, all such sums to remain available until expended for use in conjunction with a separate general request for proposals": Provided, That these actions are taken pursuant to section 202(b)(1) of Public Law 100-119 *(2 U.S.C. 909):* Provided further, That a fourth general request for proposals shall be issued not later than February 1, 1991, and a fifth general request for proposals shall be issued not later than March 1, 1992: Provided further, That project proposals resulting from such solicitations shall be selected not later than eight months after the date of the general request for proposals: Provided further, That for clean coal solicitations required herein, provisions included for the repayment of government contributions to individual projects shall be identical to those included in the Program Opportunity Notice (PON) for Clean Coal Technology III (CCT-III) Demonstration Projects (solicitation number DE-PS01-89 FE 61825), issued by the Department of Energy on May 1, 1989: Provided further, That funds provided under this head in this or any other appropriations Act shall be expended only in accordance with the provisions governing the use of such funds contained under this head in this or any other appropriations Act.

With regard to funds made available under this head in this and previous appropriations Acts, unobligated balances excess to the needs of the procurement for which they originally were made available may be applied to other procurements for use on projects for which cooperative agreements are in place, within the limitations and proportions of Government financing increases currently allowed by law: Provided, That the Department of Energy, for a period of up to five (5) years after completion of the operations phase of a cooperative agreement may provide appropriate protections, including exemptions from subchapter II of chapter 5 of title 5, United States Code, against the dissemination of information that results from demonstration activities conducted under the Clean Coal Technology Program and that would be a trade secret or commercial or financial information that is privileged or confidential if the information had been obtained from and first produced by a non-Federal party participating in a Clean Coal Technology project: Provided further, That, in addition to the full-time permanent Federal employees specified in section 303 of Public Law 97-257, as amended, no less than 90 full-time Federal employees shall be assigned to the Assistant Secretary for Fossil Energy for carrying out the programs under this head using funds available under this head in this and any other appropriations Act and of which 35 shall be for PETC and 30 shall be for METC: Provided further, That reports on projects selected by the Secretary of Energy pursuant to authority granted under this heading which are received by the Speaker of the House of Representatives and the President of the Senate less than 30 legislative days prior to the end of the second session of the 101st Congress shall be deemed to have met the criteria in the third proviso of the fourth paragraph under the heading "Administrative provisions, Department of Energy" in the Department of the Interior and Related Agencies Appropriations Act, 1986, as contained in Public Law 99-190, upon expiration of 30 calendar days from receipt of the report by the Speaker of the House of Representatives and the President of the Senate or at the end of the session, whichever occurs later.

Conference Report (H.R. Conf. Rep. No. 971, 101st Cong., 2nd Sess. [1990])

Clean Coal Technology

Amendment No. 142: Provides $35,000,000 for clean coal technology on September 1, 1991 as proposed by the House instead of $100,000,000 as proposed by the Senate. This amendment and Amendment No. 143 shift the availability of $65,000,000 from fiscal year 1991 to fiscal year 1992.

Amendment No. 143: Provides $315,000,000 for clean coal technology on October 1, 1991 as proposed by the House instead of $250,000,000 as proposed by the Senate. This amendment and Amendment No. 142 shift the availability of $65,000,000 from fiscal year 1991 to fiscal year 1992.

Amendment No. 144: Provides dates for two solicitations for clean coal technology as proposed by the Senate. The date for CCT-IV is amended to February 1, 1991 from January 1, 1991. The date for CCT-V is not changed from the Senate date of March 1, 1992.

The managers have agreed to a February 1, 1991 date for the next solicitation to enable the Department to publish a draft solicitation for comment by interested parties. It is expected that there will be changes to evaluation criteria and other factors that make it imperative that potential proposers have an opportunity to comment on the content of the solicitation.

The managers urge the Department to include potential benefits to remote, import-dependent sites as a program policy factor in evaluating proposals. The Department should also consider projects which can provide multiple fuel resource options for regions which are more than seventy-five percent dependent on one fuel form for total energy requirements.

Amendment No. 145: Requires selection of projects within eight months of the requests for proposals required by Amendment No. 144 as proposed by the Senate. The House had no such provision.

Amendment No. 146: Requires repayment of government contributions to projects under conditions identical to the most recent clean coal solicitation as proposed by the Senate. The House had no such provision.

Amendment No. 147: Provides that funds for clean coal technology may be expended only under conditions contained in appropriations Acts. The Senate language had prohibited geographic restrictions on the expenditure of funds. The House had no such provision. The managers direct that no preferential consideration be given to any project referenced explicitly or implicitly in other legislation.

The managers agree to delete bill language dealing with geographic restrictions based on such restrictions being deleted from clean air legislation.

Amendment No. 148: Earmarks employees to two fossil energy technology centers as proposed by the Senate. The House had no such provision. The managers agree that the earmarks for PETC and METC are minimum levels and may be increased as necessary.

The managers agree that no more than the current 30 full-time equivalent positions from fossil energy research and development may be used in the clean coal program in fiscal year 1991.

Public Law 102-154

Public Law 102-154, 105 Stat. 990 (1991)

Clean Coal Technology

The first paragraph under this head in Public Law 101-512 is amended by striking the phrase "$150,000,000 on October 1, 1991, $225,000,000 on October 1, 1992" and inserting "$100,000,000 on October 1, 1991, $275,000,000 on October 1, 1992".

Notwithstanding the issuance date for the fifth general request for proposals under this head in Public Law 101-512, such request for proposals shall be issued not later than July 6, 1992, and notwithstanding the proviso under this head in Public Law 101-512 regarding the time interval for selection of proposals resulting from such solicitation, project proposals resulting from the fifth general request for proposals shall be selected not later than ten months after the issuance date of the fifth general request for proposals: Provided, That hereafter the fifth general request for proposals shall be subject to all provisos contained under this head in previous appropriations Acts unless amended by this Act.

Notwithstanding the provisos under this head in previous appropriations Acts, projects selected pursuant to the fifth general request for proposals shall advance significantly the efficiency and environmental performance of coal-using technologies and be applicable to either new or existing facilities: Provided, That budget periods may be used in lieu of design, construction, and operating phases for cost-sharing calculations: Provided further, That the Secretary shall not finance more than 50 per centum of the total costs of any budget period: Provided further, That project specific development activities for process performance definition, component design verification, materials selection, and evaluation of alternative designs may be funded on a cost-shared basis up to a limit of 10 per centum of the Government's share of project cost: Provided further, That development activities eligible for cost-sharing may include limited modifications to existing facilities for project related testing but do not include construction of new facilities.

With regard to funds made available under this head in this and previous appropriations Acts, unobligated balances excess to the needs of the procurement for which they originally were made available may be applied to other procurements for use on projects for which cooperative agreements are in place, within the limitations and proportions of Government financing increases currently allowed by law: Provided, That hereafter, the Department of Energy, for a period of up to five years after completion of the operations phase of a cooperative agreement may provide appropriate protections, including exemptions from subchapter II of chapter 5 of title 5, United States Code, against the dissemination of information that results from demonstration activities conducted under the Clean Coal Technology Program and that would be a trade secret or commercial or financial information that is privileged or confidential if the information had been obtained from and first produced by a non-Federal party participating in a Clean Coal Technology project: Provided further, That hereafter, in addition to the full-time permanent Federal employees specified in section 303 of Public Law 97-257, as amended, no less than 90 full-time Federal employees shall be assigned to the Assistant Secretary for Fossil Energy for carrying out the programs under this head using funds available under this head in this and any other appropriations Act and of which not less than 35 shall be for PETC and not less than 30 shall be for METC: Provided further, That hereafter reports on projects selected by the Secretary of Energy pursuant to authority granted under this heading which are received by the Speaker of the House of Representatives and the President of the Senate less than 30 legislative days prior to the end of each session of Congress shall be deemed to have met the criteria in the third proviso of the fourth paragraph under the heading "Administrative provisions, Department of Energy" in the Department of the Interior and Related Agencies Appropriations Act, 1986, as contained in Public Law 99-190, upon expiration of 30 calendar days from receipt of the report by the Speaker of the House of Representatives and the President of the Senate or at the end of the session, whichever occurs later.

Conference Report (H.R. Conf. Rep. No. 256, 102nd Cong., 1st Sess. [1991])

Clean Coal Technology

Amendment No. 165: Reported in technical disagreement. The managers on the part of the House will offer a motion to recede and concur in the amendment of the Senate with an amendment as follows:

In lieu of the matter stricken and inserted by said amendment insert:

Notwithstanding the issuance date for the fifth general request for proposals under this head in Public Law 101-512, such request for proposals shall be issued not later than July 6, 1992, and notwithstanding the proviso under this head in Public Law 101-512 regarding the time interval for selection of proposals resulting from such solicitation, project proposals resulting from the fifth general request for proposals shall be selected not later than ten months after the issuance date of the fifth general request for proposals: Provided, That hereafter the fifth general request for proposals

The managers on the part of the Senate will move to concur in the amendment of the House to the amendment of the Senate.

The amendment changes the issuance date for the fifth general request for proposals to July 6, 1992 instead of March 1, 1992 as proposed by the House and August 10, 1992 as proposed by the Senate and the allowable length of time from issuance of the request for proposals to selection of projects to ten months. The amendment also deletes Senate proposed bill language pertaining to a sixth general request for proposals as discussed below.

The managers agree that the additional two months in the procurement process for the fifth round of proposals should include an additional month to allow for the preparation of proposals by the private sector, and up to an additional month for Department of Energy review and evaluation of proposals when compared to the process for the fourth round.

The managers have agreed to delete bill language regarding a sixth round of proposals, but agree that funding will be provided for a sixth round based on unobligated and unneeded amounts that may become available from the first five rounds. The report from the Secretary on available funds, which was originally in the Senate amendment, is still a requirement and such report should be submitted to the House and Senate Committees on Appropriations not later than May 1, 1994. Based on that report, the funding, dates and conditions for the sixth round will be included in the fiscal year 1995 appropriation.

The managers expect that the fifth solicitation will be conducted under the same general types of criteria as the fourth solicitation principally modified only (1) to include the wider range of eligible technologies or applications; (2) to adjust technical criteria to consider allowable development activities, to strengthen criteria for non-utility demonstrations, and to adjust commercial performance criteria for additional facilities and technologies with regard to aspects of general energy efficiency and environmental performance; and (3) to clarify and strengthen cost and finance criteria particularly with regard to development activities.

Amendment No. 166: Restores House language deleted by the Senate which refers to a fifth general request for proposals. The Senate proposed language dealing with both a fifth and a sixth round.

Amendment No. 167: Reported in technical disagreement. The managers on the part of the House will offer a motion to recede and concur in the amendment of the Senate which directs the Secretary of Energy to reobligate up to $44,000,000 from the fourth round of Clean Coal Technology proposals to a proposal ranked highest in its specific technology category by the Source Evaluation Board if other than the highest ranking project in that category was selected originally by the Secretary, and if such funds become unobligated and are sufficient to fund such projects. This amendment would earmark such funds, if they become available, to a specific project not chosen in the Department of Energy selection process for the fourth round of Clean Coal Technology.

Amendment No. 168: Technical amendment which deletes House proposed punctuation and numbering as proposed by the Senate.

Amendment No. 169: Deletes House proposed language which made unobligated funds available for procurements for which requests for proposals have not been issued.

Amendment No. 170: Reported in technical disagreement. The managers on the part of the House will offer a motion to recede and concur in the amendment of the Senate which adds “not less than” to employment floor language for PETC as proposed by the Senate. The House had no such language.

Amendment No. 171: Reported in technical disagreement. The managers on the part of the House will offer a motion to recede and concur in the amendment of the Senate which adds “not less than” to employment floor language for METC as proposed by the Senate. The House had no such language.

Public Law 102-381

Public Law 102-381, 106 Stat. 1374 (1992)

Clean Coal Technology

The first paragraph under this head in Public Law 101-512, as amended, is further amended by striking the phrase “and $250,000,000 on October 1, 1992” and inserting “$150,000,000 on October 1, 1993, and $100,000,000 on October 1, 1994” and by striking the phrase “$275,000,000 on October 1, 1992, and $225,000,000 on October 1, 1993” and inserting “$250,000,000 on October 1, 1993, and $250,000,000 on October 1, 1994”.

Public Law 103-138

Public Law 103-138, 107 Stat. 1379 (1993)

Clean Coal Technology

The first paragraph under this head in Public Law 101-512, as amended, is further amended by striking the phrase "$150,000,000 on October 1, 1993, and $100,000,000 on October 1, 1994" and inserting "$100,000,000 on October 1, 1993, $100,000,000 on October 1, 1994, and $50,000,000 on October 1, 1995" and by striking the phrase "$250,000,000 on October 1, 1993, and $250,000,000 on October 1, 1994" and inserting "$125,000,000 on October 1, 1993, $275,000,000 on October 1, 1994, and $100,000,000 on October 1, 1995".

Public Law 103-332

Public Law 103-332, 108 Stat. 2499 (1994)

Clean Coal Technology

The first paragraph under this head in Public Law 101-512, as amended, is further amended by striking the phrase "$100,000,000 on October 1, 1994, and $50,000,000 on October 1, 1995" and inserting "$18,000,000 on October 1, 1994, $100,000,000 on October 1, 1995, and $32,000,000 on October 1, 1996"; and by striking the phrase "$275,000,000 on October 1, 1994, and $100,000,000 on October 1, 1995" and inserting "$19,121,000 on October 1, 1994, $100,000,000 on October 1, 1995, and $255,879,000 on October 1, 1996": Provided, That not to exceed $18,000,000 available in fiscal year 1995 may be used for administrative oversight of the Clean Coal Technology program.

Public Law 104-6

Public Law 104-6, 109 Stat. 73 (1995)

Clean Coal Technology
(Rescission)

Of the funds made available under this heading for obligation in fiscal year 1996, $50,000,000 are rescinded and of the funds made available under this heading for obligation in fiscal year 1997, $150,000,000 are rescinded: Provided, That funds made available in previous appropriations Acts shall be available for any ongoing project regardless of the separate request for proposal under which the project was selected.

Public Law 104-134

Conference Report (H.R. Conf. Rep. No. 402, 104th Cong., 1st Sess. [1995])

The managers do not object to the use of up to $18,000,000 in clean coal technology program funds for administration of the clean coal program.

Public Law 104-208

Conference Report (H.R. Conf. Rep. No. 863, 104th Cong., 2nd Sess., [1996])

CLEAN COAL TECHNOLOGY
(RESCISSION)

Of the funds made available under this heading for obligation in fiscal year 1997 or prior years, $123,000,000 are rescinded: Provided, That funds made available in previous appropriations Acts shall be available for any ongoing project regardless of the separate request for proposal under which the project was selected.

Senate Report (S. Rep. No. 319, 104th Cong., 2nd Sess. [1996])

The Committee does not object to the use of up to $16,000,000 in available funds for administration of the clean coal program in fiscal year 1997.

House Report (H.R. Rep. No. 625, 104th Cong., 2nd Sess. [1996])

The Committee does not object to the use of up to $16,000,000 in available funds for administration of the clean coal program in fiscal year 1997.

Public Law 105-18

Public Law 105-18, 111 Stat. 158 (1997)

CLEAN COAL TECHNOLOGY
(RESCISSION)

Of the funds made available under this heading for obligation in fiscal year 1997 or prior years, $17,000,000 are rescinded: *Provided*, That funds made available in previous appropriations Acts shall be available for any ongoing project regardless of the separate request for proposal under which the project was selected.

Public Law 105-83

Public Law 105-83, 111 Stat. 37 (1997)

Of the funds made available under this heading for obligation in fiscal year 1997 or prior years, $101,000,000 are rescinded: *Provided*, That funds made available in previous appropriations Acts shall be available for any ogoing project regardless of the separate request for proposal under which the project was selected.

Public Law 105-277

Public Law 105-277, 112 Stat. 2681 (1998)

CLEAN COAL TECHNOLOGY
(DEFERRAL)

Of the funds made available under this heading for obligation in prior years, $10,000,000 of such funds shall not be available until October 1, 1999; $15,000,000 shall not be available until October 1, 2000; and $15,000,000 shall not be available until October 1, 2001: Provided, That funds made available in previous appropriations Acts shall be available for any ongoing project regardless of the separate request for proposal under which the project was selected.

Conference Report (H.R. Conf. Rep. No. 825, 105th Cong. 2nd Sess. [1998])

CLEAN COAL TECHNOLOGY

The conference agreement provides for the deferral of $40,000,000 in previously appropriated funds for the clean coal technology program as proposed by the Senate. The House did not propose to defer funding. The Committees agree that $14,900,000 may be used for administration of the clean coal technology program.

Appendix B: Program History

Solicitation History

The objective of the CCT-I solicitation, issued February 17, 1986, was to seek cost-shared projects to demonstrate the feasibility of clean coal technologies for commercial applications. The Program Opportunity Notice (PON) elicited 51 proposals. Nine projects were selected and 14 projects were placed on a list of alternatives in the event negotiations on the original 9 projects were unsuccessful; 8 alternate projects were eventually selected as replacement projects. Projects were selected from the list of alternates on three separate occasions.

The CCT-II PON, issued February 22, 1988, solicited cost-shared, innovative clean coal technology projects to demonstrate technologies that were capable of being commercialized in the 1990s, more cost effective than current technologies, and capable of achieving significant reductions in SO_2 and/or NO_x emissions from existing coal-burning facilities, particularly those that contribute to transboundary air pollution. The CCT-II PON was the first solicitation implementing the recommendations of the U.S. and Canadian Special Envoys' report on acid rain. DOE received 55 proposals and selected 16 as best furthering the goals and objectives of the PON (no alternates were selected).

The objective of the CCT-III PON, issued May 1, 1989, was to solicit cost-shared clean coal technology projects to demonstrate innovative, energy-efficient technologies capable of being commercialized in the 1990s. These technologies were to be capable of (1) achieving significant reductions in emissions of SO_2 and/or NO_x from existing facilities to minimize environmental impacts, such as transboundary and interstate air pollution, and/or (2) providing for future energy needs in an environmentally acceptable manner. DOE received 48 proposals and selected 13 projects as best furthering the goals and objectives of the PON.

The CCT-IV PON, issued January 17, 1991, solicited proposals to conduct cost-shared clean coal technology projects to demonstrate innovative, energy-efficient, economically competitive technologies. These technologies were to be capable of (1) retrofitting, repowering, or replacing existing facilities while achieving significant reductions in the emissions of SO_2, NO_x, or both and/or (2) providing for future energy needs in an environmentally acceptable manner. A total of 33 proposals were submitted in response to the PON. Nine projects were selected.

The objective of the CCT-V PON, issued July 6, 1992, was to solicit proposals to conduct cost-shared demonstration projects that significantly advance the efficiency and environmental performance of coal-using technologies and are applicable to either new or existing facilities. In response to the solicitation, DOE received proposals for 24 projects and selected 5 projects.

Selection and Negotiation History

July 1986
Nine projects were selected under CCT-I (14 alternate projects selected to replace any selected projects if negotiations were unsuccessful).

March 1987
DOE signed cooperative agreements with two CCT-I participants, Coal Tech Corporation (Advanced Cyclone Combustor with Internal Sulfur, Nitrogen, and Ash Control) and The Ohio Power Company (Tidd PFBC Demonstration Project).

June 1987
DOE signed a cooperative agreement with CCT-I participant, The Babcock & Wilcox Company (LIMB Demonstration Project Extension and Coolside Demonstration).

July 1987
DOE signed a cooperative agreement with CCT-I participant, Energy and Environmental Research Corporation (Enhancing the Use of Coals by Gas Reburning and Sorbent Injection).

September 1987
General Electric Company withdrew its proposal (Integrated Coal Gasification Steam Injection Gas Turbine Demonstration Plants with Hot Gas Cleanup).

October 1987
Weirton Steel Corporation withdrew its proposal, Direct Iron Ore Reduction to Replace Coke Oven/ Blast Furnace for Steelmaking, from further consideration.

Four more CCT-I projects were selected: Colorado-Ute Electric Association, Inc. (Nucla CFB Demonstration Project); TRW, Inc. (Advanced Slagging Coal Combustor Utility Demonstration Project); Minnesota Department of Natural Resources (COREX Ironmaking Demonstration Project); and Foster Wheeler Power Systems, Inc. (Clean Energy IGCC Demonstration Project).

December 1987
DOE signed cooperative agreements with two more CCT-I participants, Ohio Ontario Clean Fuels, Inc., (Prototype Commercial Coal/Oil Coprocessing Project) and Energy International, Inc. (Underground Coal Gasification Demonstration Project).

January 1988
DOE signed a cooperative agreement with The M.W. Kellogg Company and Bechtel Development Company for a CCT-I project, The Appalachian IGCC Demonstration Project.

September 1988
Sixteen projects were selected under CCT-II.

November 1988
DOE signed a cooperative agreement with CCT-I participant, TRW, Inc. (Advanced Slagging Coal Combustor Utility Demonstration Project).

December 1988
Negotiations were terminated with Minnesota Department of Natural Resources (COREX Ironmaking Demonstration Project) under CCT-I.

DOE selected three more CCT-I projects: ABB Combustion Engineering, Inc., and CQ Inc. (Development of the Coal Quality Expert); Western Energy Company (now Rosebud SynCoal Partnership; Advanced Coal Conversion Process Demonstration); and United Coal Company (Coal Waste Recovery Advanced Technology Demonstration).

June 1989
The City of Tallahassee CCT-I project, ACFB Repowering, was selected from the alternate list.

The M.W. Kellogg Company and Bechtel Development Company withdrew their CCT-I project, Clean Energy IGCC Demonstration Project.

September 1989
United Coal Company withdrew its CCT-I project, Coal Waste Recovery Advanced Technology Demonstration.

November 1989
DOE signed a cooperative agreement with CCT-II participant, Bethlehem Steel Corporation (Innovative Coke Oven Gas Cleaning System for Retrofit Applications).

Combustion Engineering, Inc., (CCT-II) withdrew its Postcombustion Sorbent Injection Demonstration Project.

December 1989
Thirteen projects were selected under CCT-III.

DOE signed cooperative agreements with five CCT-II participants: ABB Combustion Engineering, Inc. (SNOX™ Flue Gas Cleaning Demonstration Project); The Babcock & Wilcox Company (SO_x-NO_x-Rox Box™ Flue Gas Cleanup Demonstration Project); Passamaquoddy Tribe (Cement Kiln Flue Gas Recovery Scrubber); Pure Air on the Lake, L.P. (Advanced Flue Gas Desulfurization Demonstration Project); and Southern Company Services, Inc. (Demonstration of Advanced Combustion Techniques for a Wall-Fired Boiler).

Energy International, Inc., withdrew its CCT-I project, Underground Coal Gasification Demonstration Project.

February 1990
Foster Wheeler Power Systems, Inc., withdrew its CCT-I proposal, Clean Energy IGCC Demonstration Project.

April 1990

DOE signed cooperative agreements with three CCT-II participants: The Appalachian Power Company (PFBC Utility Demonstration Project); The Babcock & Wilcox Company (Demonstration of Coal Reburning for Cyclone Boiler NO_x Control); and Southern Company Services, Inc. (Demonstration of Innovative Applications of Technology for the CT-121 FGD Process).

June 1990

DOE signed cooperative agreements with the co-participants of one CCT-I project, ABB Combustion Engineering, Inc., and CQ Inc., (Development of the Coal Quality Expert™) and with two CCT-II participants: Southern Company Services, Inc. (Demonstration of Selective Catalytic Reduction Technology for the Control of NO_x Emissions from High-Sulfur-Coal-Fired Boilers) and TransAlta Resources Investment Corporation (LNS Burner for Cyclone-Fired Boilers Demonstration Project).

September 1990

DOE signed cooperative agreements with one CCT-I participant, Western Energy Company (now Rosebud SynCoal Partnership; Advanced Coal Conversion Process Demonstration); one CCT-II participant, Southern Company Services, Inc. (180-MWe Demonstration of Advanced Tangentially Fired Combustion Techniques for the Reduction of NO_x Emissions from Coal-Fired Boilers); and one CCT-III participant, ENCOAL Corporation (ENCOAL® Mild Coal Gasification Project).

Negotiations were terminated with CCT-II participant, Southwestern Public Service Company (Nichols CFB Repowering Project).

October 1990

DOE signed cooperative agreements with four CCT-III participants: AirPol, Inc. (10-MWe Demonstration of Gas Suspension Absorption); The Babcock & Wilcox Company (Full-Scale Demonstration of Low-NO_x Cell Burner Retrofit); Bechtel Corporation (Confined Zone Dispersion Flue Gas Desulfurization Demonstration); and Energy and Environmental Research Corporation (Evaluation of Gas Reburning and Low-NO_x Burners on a Wall-Fired Boiler).

November 1990

DOE signed cooperative agreements with one CCT-I participant, The City of Tallahassee (Arvah B. Hopkins Circulating Fluidized-Bed Repowering Project; now JEA); one CCT-II participant, ABB Combustion Engineering, Inc. (Combustion Engineering IGCC Repowering Project); and two CCT-III participants, Bethlehem Steel Corporation (Blast Furnace Granular-Coal Injection System Demonstration Project) and LIFAC-North America (LIFAC Sorbent Injection Desulfurization Demonstration Project).

December 1990

Negotiations terminated with CCT-II participant, Otisca Industries, Ltd. (Otisca Fuel Demonstration Project).

March 1991

DOE signed cooperative agreements with three CCT-III participants: MK-Ferguson Company (now NOXSO Corporation; Commercial Demonstration of the NOXSO SO_2/NO_x Removal Flue Gas Cleanup System); Public Service Company of Colorado (Integrated Dry NO_x/SO_2 Emissions Control System); and Tampa Electric Company (formerly Clean Power Cogeneration Limited Partnership; Tampa Electric Integrated Gasification Combined-Cycle Project).

TRW, Inc., withdrew its CCT-I project (Advanced Slagging Coal Combustion Utility Demonstration Project).

April 1991

DOE signed a cooperative agreement with CCT-III participant, Alaska Industrial Development and Export Authority (Healy Clean Coal Project).

June 1991

DOE withdrew its sponsorship of the Ohio Ontario Clean Fuels, Inc., CCT-I project, Prototype Commercial Coal/Oil Coprocessing Plant.

August 1991

DOE signed a cooperative agreement with CCT-III participant, DMEC-1 Limited Partnership (formerly Dairyland Power Cooperative; PCFB Demonstration Project).

TransAlta Resources Investment Corporation withdrew its CCT-II project, LNS Burner for Cyclone-Fired Boilers Demonstration Project.

September 1991
Nine projects were selected under CCT-IV.

Coal Tech Corporation's CCT-I project, Advanced Cyclone Combustor with Internal Sulfur, Nitrogen, and Ash Control, final reports issued and project completed.

April 1992
Tri-State Generation and Transmission Association, Inc.'s (formerly Colorado-Ute Electric Association, Inc.) CCT-I project, Nucla CFB Demonstration Project, final reports issued and project completed.

June 1992
The City of Tallahassee project (CCT-I) was restructured and transferred to York County Energy Partners, L.P. (York County Energy Partners Cogeneration Project).

July 1992
DOE signed cooperative agreements with two CCT-IV participants: Tennessee Valley Authority (now New York State Electric & Gas Corporation project; Micronized Coal Reburning Demonstration for NO_x Control on a 175-MWe Wall-Fired Unit), and the Wabash River Coal Gasification Repowering Project Joint Venture (Wabash River Coal Gasification Repowering Project).

August 1992
DOE signed a cooperative agreement with CCT-IV participant, Sierra Pacific Power Company (Piñon Pine IGCC Power Project).

Cordero Mining Company withdrew from negotiations for its CCT-IV project, Cordero Coal-Upgrading Demonstration Project.

At the participant's request, Union Carbide Chemicals and Plastics Company Inc. (CCT-IV) was granted an extension of one year to the DOE deadline for completing negotiations of its Demonstration of the Union Carbide CANSOLVT System at the Alcoa Generating Corporation Warrick Power Plant.

October 1992
DOE signed cooperative agreements with one CCT-III participant, Air Products and Chemicals, Inc. (Commercial-Scale Demonstration of the Liquid-Phase Methanol [LPMEOH™] Process) and with four CCT-IV participants: Custom Coals International (Self-Scrubbing Coal™: An Integrated Approach to Clean Air); New York State Electric & Gas Corporation (Milliken Clean Coal Technology Demonstration Project); TAMCO Power Partners (Toms Creek IGCC Demonstration Project); and ThermoChem, Inc. (Demonstration of Pulse Combustion in an Application for Steam Gasification of Coal).

November 1992
The Babcock & Wilcox Company's CCT-I project, LIMB Demonstration Project Extension and Coolside Demonstration, final reports issued and project completed.

May 1993
Five projects were selected under CCT-V: Four Rivers Energy Partners, L.P. (Four Rivers Energy Modernization Project (formerly Calvert City Advanced Energy Project, now McIntosh Unit 4B Topped PCFB Demonstration Project); Duke Energy Corp. (Camden Clean Energy Demonstration Project); Centerior Energy Corporation, on behalf of CPICOR™ Management Company L.L.C. (Clean Power from Integrated Coal/Ore Reduction [CPICOR™]); Arthur D. Little, Inc. (Clean Coal Combined-Cycle Project; previously Demonstration of Coal Diesel Technology at Easton Utilities); and Pennsylvania Electric Company (Warren Station Externally Fired Combined-Cycle Demonstration Project).

July 1993
Union Carbide Chemicals and Plastics Company, Inc., withdrew its CCT-IV proposal, Demonstration of the Union Carbide CANSOLVT System at the Alcoa Generating Corporation Warrick Power Plant.

February 1994
The Passamaquoddy Tribe's CCT-III project, Cement Kiln Flue Gas Recovery Scrubber, final reports issued and project completed.

March 1994
The Babcock & Wilcox Company's CCT-II project, Demonstration of Coal Reburning for Cyclone Boiler NO_x Control, final reports issued and project completed.

June 1994

DOE signed a cooperative agreement with CCT-V participant, Arthur D. Little, Inc. (Coal Diesel Combined-Cycle Project).

Southern Company Services' CCT-III project, 180-MWe Demonstration of Advanced Tangentially Fired Combustion Techniques for the Reduction of NO_x Emissions from Coal-Fired Boilers, final reports issued and project completed.

Bechtel Corporation's CCT-III project, Confined Zone Dispersion Flue Gas Desulfurization Demonstration, final reports issued and project completed.

August 1994

DOE signed cooperative agreements with two CCT-V participants, Four Rivers Energy Partners, L.P. (Four Rivers Energy Modernization Project); and Pennsylvania Electric Company (Warren Station Externally Fired Combined-Cycle Demonstration Project).

The CCT-III project, Commercial Demonstration of the NOXSO SO_2/NO_x Removal Flue Gas Cleanup System, was relocated and transferred to NOXSO Corporation.

September 1994

The Air Products and Chemicals CCT-III project, Commercial-Scale Demonstration of the Liquid-Phase Methanol (LPMEOH™) Process, was transferred to Air Products Liquid Phase Conversion Company, L.P.

December 1994

DOE signed a cooperative agreement with CCT-V participant, Clean Energy Partners Limited Partnership (formerly Duke Energy Corp.; Clean Energy Demonstration Project).

March 1995

TAMCO Power Partner's CCT-IV project, Toms Creek IGCC Demonstration Project, was not granted a further extension and the project was concluded.

April 1995

Bethlehem Steel Corporation's CCT-II project, Innovative Coke Oven Gas Cleaning System for Retrofit Applications, was terminated by mutual agreement with DOE because coke production was suspended at the demonstration facility.

June 1995

AirPol, Inc.'s CCT-II project, 10-MWe Demonstration of Gas Suspension Absorption, final reports issued and project completed.

September 1995

The Babcock & Wilcox Company's CCT-II project, SO_x-NO_x-Rox Box™ Flue Gas Cleanup Demonstration Project, final reports issued and project completed.

December 1995

The Tennessee Valley Authority and New York State Electric & Gas Corporation finalized an agreement to allow the project, Micronized Coal Reburning Demonstration for NO_x Control, to be conducted at both Milliken Station in Lansing, NY, and Eastman Kodak Company in Rochester, NY.

The Babcock & Wilcox Company's CCT-II project, Full-Scale Demonstration of Low-NO_x Cell Burner Retrofit, final reports issued and project completed.

The Ohio Power Company's CCT-I project, Tidd PFBC Demonstration Project, final reports issued and project completed.

May 1996

The ABB Combustion Engineering, Inc., CCT-II project, Combustion Engineering IGCC Repowering Project, was concluded.

June 1996

Pure Air on the Lake's CCT-II project, Advanced Flue Gas Desulfurization Project, final reports issued and project completed.

August 1996

The Arthur D. Little, Inc., CCT-V project was restructured and retitled as the Clean Coal Diesel Demonstration Project.

September 1996
The Appalachia Power Company CCT-II project, PFBC Utility Demonstration Project, was concluded.

October 1996
DOE signed a cooperative agreement with CCT-V participant, CPICOR™ Management Company, L.L.C. (Clean Power from Integrated Coal/Ore Reduction [CPICOR™]).

November 1996
Southern Company Services' CCT-II project, Demonstration of Selective Catalytic Reduction Technology for the Control of NO_x Emissions from High-Sulfur Coal-Fired Boilers, final reports issued and project completed.

December 1996
ABB Environmental Systems' CCT-II project, SNOX™ Flue Gas Cleaning Demonstration Project, final reports issued and project completed.

May 1997
The Pennsylvania Electric Company CCT-V project, Externally Fired Combined-Cycle Demonstration Project, was concluded.

September 1997
DOE modified the cooperative agreement for JEA's CCT-I project, JEA Large-Scale CFB Combustion Project (formerly The City of Tallahassee project, then the York County Energy Partners project).

December 1997
ENCOAL Corporation's CCT-III project, ENCOAL® Mild Coal Gasification Project, final reports issued and project completed.

DOE signed a new cooperative agreement for the restructured City of Lakeland's CCT-III project, McIntosh Unit 4A PCFB Demonstration Project (formerly the DMEC-1 Limited Partnership project).

January 1998
DOE signed a new cooperative agreement for the restructured City of Lakeland's CCT-III project, McIntosh Unit 4B Topped PCFB Demonstration Project (formerly the Four Rivers Energy Partners, L.P. project).

April 1998
LIFAC-North America's CCT-III project, LIFAC Sorbent Injection Desulfurization Project, final reports issued and project completed.

June 1998
Southern Company Services, Inc.'s CCT-II project, Demonstration of Advanced Combustion Techniques for a Wall-Fired Boiler, final report issued and project completed.

Southern Company Services' CCT-II project, Demonstration of Innovative Applications of Technology for the CT-121 FGD Process, final reports issued and project completed.

The ABB Combustion Engineering, Inc., and CQ Inc.'s CCT-I project, Development of the Coal Quality Expert™, final reports issued and project completed.

September 1998
Energy and Environmental Research Corporation's CCT-I project, Enhancing the Use of Coals by Gas Reburning and Sorbent Injection, final reports issued and project completed.

DOE signed a revised cooperative agreement with for the restructured ThermoChem Inc.'s CCT IV project, Pulse Combustion Design Qualification test.

October 1998
Energy and Environmental Research Corporation's CCT III project, Evaluation of Gas Reburning and Low-NO_x Burners on a Wall-Fired Boiler, final reports issued and project completed.

Appendix C: Environmental Aspects

Introduction

The U.S. Department of Energy employs a three-step process to ensure that the CCT Program and its projects comply with the procedural requirements of the National Environmental Policy Act (NEPA) and the regulations for NEPA compliance promulgated by the Council on Environmental Quality (CEQ) (40 CFR Parts 1500–1508) and by DOE (10 CFR Part 1021). This process includes (1) preparation of a programmatic environmental impact statement (PEIS) in 1989; (2) preparation of preselection, project-specific environmental reviews; and (3) preparation of postselection, site-specific NEPA documentation. Several types of NEPA documents have been used in the CCT Program, including memoranda-to-file (MTF; discontinued as of September 30, 1990), environmental assessments (EA), and environmental impact statements (EIS). The Department of Energy's NEPA regulations also provide for categorical exclusions (CX) for certain classes of actions.

Exhibit C-1 shows the progress made through September 30, 1998, to complete NEPA reviews of projects in the CCT Program. By September 30, 1998, NEPA reviews were completed for 35 of the 40 CCT projects remaining in the program (two NEPA reviews were completed for one project, Enhancing the Use of Coals by Gas Reburning and Sorbent Injection—an MTF was completed for the Hennepin site and an EA for the Lakeside site). From 1987 through September 30, 1998, NEPA requirements were satisfied with a CX for 1 project, MTFs for 17 projects, EAs for 18 projects and EISs for 4 projects (actions exceed 33 because of project terminations, withdrawals, and restructuring).

For each project cofunded by DOE under the CCT Program, the industrial participant is required to develop an environmental monitoring plan (EMP) that will ensure operational compliance and that significant technical and environmental data are collected and disseminated. Data to be collected include compliance data to meet federal, state, and local requirements and performance data to aid in future commercialization of the technology.

The Role of NEPA in the CCT Program

NEPA was initially enacted in 1969 as Public Law 91-190 and has been amended from time-to-time by Congress. The applicability of NEPA to the CCT Program is encapsulated in the following provision (Section 102):

> [A]ll agencies of the Federal Government shall—. . .
>
> (C) include in every recommendation or report on proposals for legislation and other major Federal actions significantly affecting the quality of the human environment, a detailed statement by the responsible official on—
>
> i. the environmental impact of the proposed action,
>
> ii. any adverse environmental effects which cannot be avoided should the proposal be implemented,
>
> iii. alternatives to the proposed action,
>
> iv. the relationship between local short-term uses of man's environment and the maintenance and enhancement of long-term productivity, and
>
> v. any irreversible and irretrievable commitments of resources which would be involved in the proposed action should it be implemented. . . .
>
> (E) study, develop, and describe appropriate alternatives to recommended courses of action in any proposal which involves unresolved conflicts concerning alternative uses of available resources[.]

Through NEPA, Congress created the CEQ, which has promulgated regulations that ensure compliance with the act.

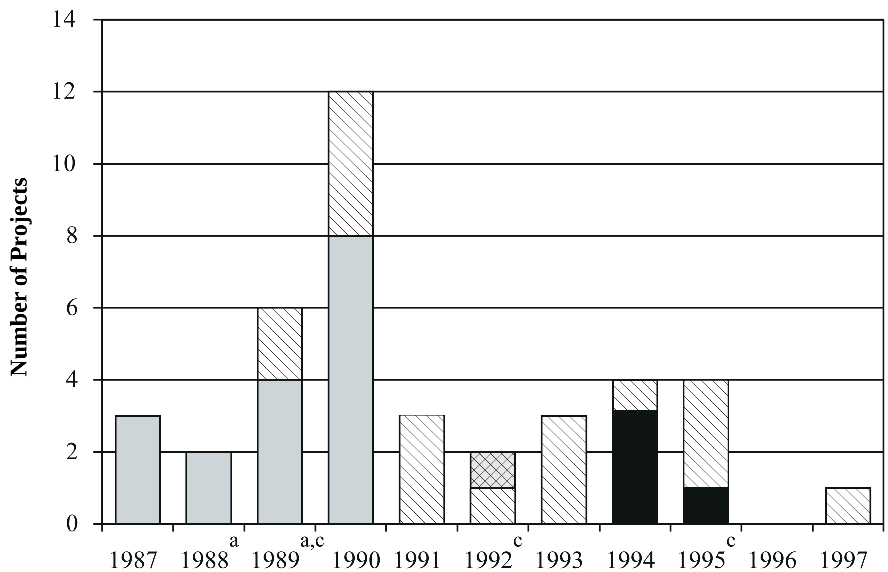
Compliance with NEPA

In November 1989, a PEIS was completed for the CCT Program. This PEIS addressed issues such as potential global climatic modification and the ecological and socioeconomic impacts of the CCT Program. The PEIS evaluated the following two alternatives:

- "No action," which assumed that conventional coal-fired technologies with conventional flue gas desulfurization controls would continue to be used, and
- "Proposed action," which assumed that successfully demonstrated clean coal technologies would undergo widespread commercialization by the year 2010.

In preselection project-specific environmental reviews, DOE evaluates the environmental aspects of

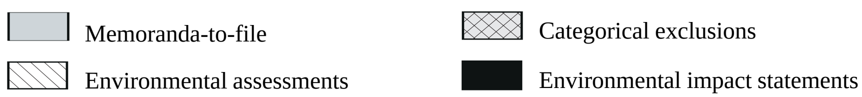
Exhibit C-1
NEPA Reviews Completed through September 30, 1998



[a] Includes an MTF (1988) and an EA (1989) required for one project

[b] Includes an EA for a project that was withdrawn

[c] Includes an EA for a project that was terminated



each proposed demonstration project. Reviews are provided to the Source Selection Official for consideration in the project selection process. The site-specific environmental, health, safety, and socioeconomic issues associated with each proposed project are examined during the NEPA review. As part of the comprehensive evaluation prior to selecting projects, the strengths and weaknesses of each proposal are compared with the environmental evaluation criteria. To the maximum extent possible, the environmental impacts of each proposed project and practical mitigating measures are considered. Also, a list of necessary permits is prepared, to the extent known; these are permits that would need to be obtained in implementing the proposed project.

Upon selection, project participants are required to prepare and submit additional environmental information. This detailed site- and project-specific information is used, along with independent information gathered by DOE, as the basis for site-specific NEPA documents which are prepared by DOE for each selected project. These NEPA documents are prepared, considered, and published in full conformance with CEQ and DOE regulations for NEPA compliance.

Categorical Exclusions

"Subpart D—Typical Classes of Actions" of the DOE NEPA regulations provide for categorical exclusions as a class of actions that DOE has determined do not individually or cumulatively have a significant effect on the human environment. One project, Micronized Coal Reburning Demonstration for NO_x Control, was covered by a categorical exclusion (NEPA review was completed August 13, 1992).

Memoranda-to-File

The MTF was established when DOE's NEPA guidelines were first issued in 1980. The MTF was intended for circumstances when the expected impacts of the proposed action were clearly insignificant, yet the action had not been specified as a categorical exclusion from NEPA documentation. The use of the MTF was terminated as of September 30, 1990. Exhibit C-2 lists the 17 projects for which an MTF was prepared.

Environmental Assessments

An EA has the following three functions:

1. To provide sufficient evidence and analysis for determining whether a proposed action requires preparation of an EIS or a finding of no significant impact (FONSI);

2. To aid an agency's compliance with NEPA when no EIS is necessary, i.e., to provide an interdisciplinary review of proposed actions, assess potential impacts, and help identify better alternatives and mitigation measures; and
3. To facilitate preparation of an EIS when one is necessary.

An EA's contents are determined on a case-by-case basis and depend on the nature of the action. If appropriate, a DOE EA also includes any floodplain or wetlands assessment that has been prepared and may include analyses needed for other environmental determinations.

If an agency determines on the basis of an EA that it is not necessary to prepare an EIS, a FONSI is issued. Council on Environmental Quality regulations describe the FONSI as a document that briefly presents the reasons why an action will not have a significant effect on the human environment and for which an EIS therefore will not be prepared. The FONSI includes the EA, or a summary of it, and notes any other related environmental documents. The CEQ and DOE regulations also provide for notification of the public that a FONSI has been issued. Also, DOE provides copies of the EA and FONSI to the public on request.

Exhibit C-3 lists the 18 projects for which an EA has been prepared. The exhibit includes EAs for one project that was subsequently withdrawn from the program—TransAlta Resources Investment Corporation's Low-NO_x/SO_2 Burner Retrofit for Utility Cyclone Boilers project—and three that were terminated—ABB Combustion Engineering's Combustion Engineering IGCC Repowering Project, Bethlehem Steel Corporation's Innovative Coke Oven Gas

Exhibit C-2
Memoranda-to-File Completed

Project and Participant	Completed
CCT-I	
Development of the Coal Quality Expert (ABB Combustion Engineering, Inc., and CQ Inc.)	4/27/90
LIMB Demonstration Project Extension and Coolside Demonstration (The Babcock & Wilcox Company)	6/2/87
Advanced Cyclone Combustor with Internal Sulfur, Nitrogen, and Ash Control (Coal Tech Corporation)	3/26/87
Nucla CFB Demonstration Project (Colorado-Ute Electric Association, Inc.; now Tri-State Generation and Transmission Association, Inc.)	4/18/88
Enhancing the Use of Coals by Gas Reburning and Sorbent Injection (Hennepin site) (Energy and Environmental Research Corporation)	5/9/88
Tidd PFBC Demonstration Project (The Ohio Power Company)	3/5/87
CCT-II	
SNOX™ Flue Gas Cleaning Demonstration Project (ABB Environmental Systems)	1/31/90
SO_x-NO_x-Rox Box™ Flue Gas Cleanup Demonstration Project (The Babcock & Wilcox Company)	9/22/89
Demonstration of Advanced Combustion Techniques for a Wall-Fired Boiler (Southern Company Services, Inc.)	5/22/89
Demonstration of Selective Catalytic Reduction Technology for the Control of NO_x Emissions from High-Sulfur-Coal-Fired Boilers (Southern Company Services, Inc.)	8/16/89
180-MWe Demonstration of Advanced Tangentially Fired Combustion Techniques for the Reduction of NO_x Emissions from Coal-Fired Boilers (Southern Company Services, Inc.)	7/21/89
CCT-III	
10-MWe Demonstration of Gas Suspension Absorption (AirPol, Inc.)	9/21/90
Full-Scale Demonstration of Low-NO_x Cell Burner Retrofit (The Babcock & Wilcox Company)	8/10/90
Confined Zone Dispersion Flue Gas Desulfurization Demonstration (Bechtel Corporation)	9/25/90
Evaluation of Gas Reburning and Low-NO_x Burners on a Wall-Fired Boiler (Energy and Environmental Research Corporation)	9/6/90
LIFAC Sorbent Injection Desulfurization Demonstration Project (LIFAC–North America)	10/2/90
Integrated Dry NO_x/SO_2 Emissions Control System (Public Service Company of Colorado)	9/27/90

Exhibit C-3
Environmental Assessments Completed

Project and Participant	Completed
CCT-I	
Enhancing the Use of Coals by Gas Reburning and Sorbent Injection (Lakeside site) (Energy and Environmental Research Corporation)	6/25/89
Advanced Coal Conversion Process Demonstration (Rosebud SynCoal Partnership)	3/27/91
CCT-II	
Combustion Engineering IGCC Repowering Project (ABB Combustion Engineering, Inc.) (project terminated)	3/27/92
Demonstration of Coal Reburning for Cyclone Boiler NO_x Control (The Babcock & Wilcox Company)	2/12/91
Innovative Coke Oven Gas Cleaning System for Retrofit Applications (Bethlehem Steel Corporation) (project terminated)	12/22/89
Cement Kiln Flue Gas Recovery Scrubber (Passamaquoddy Tribe)	2/16/90
Advanced Flue Gas Desulfurization Demonstration Project (Pure Air on the Lake, L.P.)	4/16/90
Demonstration of Innovative Applications of Technology for the CT-121 FGD Process (Southern Company Services, Inc.)	8/10/90
Low-NO_x/SO_2 Burner Retrofit for Utility Cyclone Boilers (TransAlta Resources Investment Corporation) (project withdrawn)	3/21/91
CCT-III	
Commercial-Scale Demonstration of the Liquid-Phase Methanol (LPMEOH™) Process (Air Products Liquid Phase Conversion Company, L.P.)	6/30/95
Blast Furnace Granular-Coal Injection System Demonstration Project (Bethlehem Steel Corporation)	6/8/93
ENCOAL® Mild Coal Gasification Project (ENCOAL Corporation)	8/1/90
Commercial Demonstration of the NOXSO SO_2/NO_x Removal Flue Gas Cleanup System (NOXSO Corporation)	6/26/95
CCT-IV	
Self-Scrubbing Coal™: An Integrated Approach to Clean Air (Custom Coals International)	2/14/94
Milliken Clean Coal Technology Demonstration Project (New York State Electric & Gas Corporation)	8/18/93
Warren Station Externally Fired Combined-Cycle Demonstration Project (Pennsylvania Electric Company) (Warren Station site) (project terminated)	5/18/95
Wabash River Coal Gasification Repowering Project (Wabash River Coal Gasification Repowering Project Joint Venture)	5/28/93
CCT-V	
Clean Coal Diesel Demonstration Project (Arthur D. Little, Inc.)	6/2/97

Cleaning System for Retrofit Applications and Pennsylvania Electric's Warren Station Externally Fired Combined-Cycle Demonstration Project.

Environmental Impact Statements

The primary purpose of an EIS is to serve as an action-forcing device to ensure that the policies and goals defined in NEPA are infused into the programs and actions of the federal government. An EIS contains a full and fair discussion of all significant environmental impacts. The EIS should inform decision makers and the public of reasonable alternatives that would avoid or minimize adverse impacts or enhance the quality of the human environment.

The CEQ regulations state that an EIS is to be more than a disclosure document; it is to be used by federal officials in conjunction with other relevant material to plan actions and make decisions. Analysis of alternatives is to encompass those alternatives to be considered by the ultimate decision-maker, including a complete description of the proposed action. In short, the EIS is a means of assessing the environmental impacts of a proposed DOE action, rather than justifying decisions already made, prior to making a decision to proceed with the proposed action. Consequently, before a record of decision (ROD) is issued, DOE may not take any action that would have an adverse environmental effect or limit the choice of reasonable alternatives. EISs for three projects were completed in 1994. In 1995, DOE issued a ROD on the EIS prepared for the York County Energy Partners project located in York County, Pennsylvania. However, because this project has been restructured, a new NEPA compliance document will be required for the JEA project site. (See Exhibit C-4).

Exhibit C-4
Environmental Impact Statements Completed

Project and Participant	Completed*
CCT-I	
York County Energy Partners Cogeneration Project (York County, PA site) (York County Energy Partners, L.P.)	8/11/95
CCT-III	
Healy Clean Coal Project (Alaska Industrial Development and Export Authority)	3/10/94
Tampa Electric Company Integrated Gasification Combined-Cycle Project (Tampa Electric Company)	8/17/94
CCT-IV	
Piñon Pine IGCC Power Project (Sierra Pacific Power Company)	11/8/94

* Completion is the date DOE issued a record of decision.

NEPA Actions in Progress

Exhibit C-5 lists the status of projects for which the NEPA process has not yet been completed.

Environmental Monitoring

CCT project participants are required to develop and implement an EMP which addresses both compliance and supplemental monitoring. Exhibit C-6 lists the status of EMPs for all 40 projects in the CCT Program. The EMP is intended to ensure collection and dissemination of the significant technology-, project-, and site-specific environmental data necessary for evaluation of impacts upon health, safety, and the environment. Further, the data are used to characterize and quantify the environmental performance of the technology in order to evaluate its commercialization and deployment potential. In addition to regulatory compliance data, further monitoring is required to fulfill the following:

- Ensure that emissions, ambient levels of pollutants, and environmental impacts do not exceed expectations projected in the NEPA documents,
- Identify any need for corrective action,
- Verify the implementation of any mitigative measure that may have been identified in a mitigation action plan pursuant to the provisions of an EA or EIS, and

Exhibit C-5
NEPA Reviews in Progress

Project and Participant	Status
CCT-I	
JEA Large-Scale CFB Combustion Demonstration Project	EIS planned (10/99)
CCT-III	
McIntosh Unit 4A PCFB Demonstration Project (City of Lakeland, Lakeland Electric)	EIS planned (10/99)
CCT-V	
McIntosh Unit 4B Topped PCFB Demonstration Project (City of Lakeland, Lakeland Electric)	EIS planned (10/99)
Clean Power from Integrated Coal/Ore Reduction (CPICOR™) (CPICOR™ Management Company, L.L.C.)	EIS planned (12/00)
Clean Energy Demonstration Project (Clean Energy Partners Limited Partnership)	To be determined

- Provide the essential data on the environmental performance of the technology needed to evaluate the potential impact of future commercialization, including the ability of the technology to meet requirements of the Clean Air Act and the 1990 amendments.

The objective of the CCT Program's environmental monitoring efforts is to ensure that, when commercially available, clean coal technologies will be capable of responding fully to air toxics regulations that emerge from the CAAA, and to the maximum extent possible, are in the vanguard of cost-effective solutions to concerns about public health and safety related to coal use.

Air Toxics

Title III of the CAAA lists known hazardous air pollutants (HAPs) and, among other things, calls for the EPA to establish categories of sources that emit these pollutants. Exploratory analyses suggest that HAPs may be released by conventional coal-fired power plants and, presumably, by plants using clean coal technologies. It is expected that emissions standards will be proposed for the electric-power-production-source categories. However, there are many uncertainties as to which HAPs will be regulated, their prevalence in various types and sources of coal, and their nature and fate as functions of combustion characteristics and the particular clean coal technology used.

The CCT Program recognizes the importance of monitoring HAPs in achieving widespread commercialization in the late 1990s and beyond. For all projects with existing cooperative agreements, DOE sought to include HAPs monitoring. A total of 21 projects contain provisions for monitoring HAPs.

The CCT-V Program Opportunity Notice (PON) acknowledged the importance of HAPs throughout the solicitation, including them as an aspect of proposal evaluation. The PON addressed the control of air toxics as an environmental performance criterion. Also, in the instructions on proposal preparation, the PON directed proposers as follows:

> With respect to emission of air toxics, Proposers should consider . . . the particular elements and compounds [listed in Table 5-1 of the PON, "Specific Air Toxics to be Monitored"]. Proposers should present any information known concerning the reduction of emissions of these toxics by [the proposed] technology. Some of the toxics for which the proposed technology may offer control are likely unregulated in the target market at present. The significance and importance of the additional control afforded by the proposed technology for the continued use of coal should be explained. An example of this kind would be one or more particular air toxic compounds controlled by a technology meant for use in power generation.

The CCT-V PON also stipulates that information on air toxics be presented in the environmental information required by DOE. Exhibit C-7 lists the 21 projects that provide for HAPs monitoring. Eleven of these projects have completed the HAPs monitoring requirements. The objective of the HAPs monitoring program is to improve the quality of HAPs data being gathered and to monitor a broader range of plant configurations and emissions control equipment.

The CCT Program is coordinating with organizations such as the Electric Power Research Institute (EPRI) and the Ohio Coal Development Office in activities focused on HAPs monitoring and analysis. Further, under the DOE Coal R&D Program, two reports summarizing the source, distribution, and fate of HAPs from coal-fired power plants were published in 1996. A report released in July 1996, *Summary of Air Toxics Emissions Testing at Sixteen Utility Plants*, provided assessment of HAPs measured in the coal, across the major pollution control devices, and the HAPs emitted from the stack. A second report, *A Comprehensive Assessment of Toxics Emissions from Coal-Fired Power Plants: Phase I Results from the U.S. Department of Energy Study*, was released in September 1996 and provided the raw data from the emissions testing. Emissions data were collected from 16 power plants, representing nine process configurations, operated by eight different utilities; several power plants were sites for CCT Program projects. The power plants represented a range of different coal types, process configurations, furnace types, and pollution control methods.

The second phase of the DOE/EPRI effort currently in progress is sampling at other sites, including the CCT Program's Wabash River IGCC project. Further, the results from the first phase will be used to determine what configuration and coal types require further assessment.

In October 1996, EPA submitted to Congress an interim version of its technical assessment of toxic air pollutant emissions from power plants, *Study of Hazardous Air Pollutant Emissions from Electric Utility Steam Generating Units, Interim Final Report.* EPA plans to continue evaluating the potential exposures and potential public health concerns from mercury emissions from utilities. In addition, the agency will evaluate information on various potential control technologies for mercury. If EPA decides that HAPs pose a risk, then the agency must propose air toxic emissions controls by November 15, 1998, and make them final two years later.

Following up on the October 1996 report to Congress, a report was released by EPA focusing on Mercury emissions. The December 1997 report, *Mercury Study Report to Congress*, estimates the U.S. industrial sources were responsible for releasing 158 tons of Mercury into the atmosphere in 1994 and 1995. The EPA estimates that 87 percent of those emissions originate from combustion sources such as waste and fossil fuel facilities, 10 percent from manufacturing facilities, 2 percent from area sources, and 1 percent from other sources. The EPA also identified four specific categories that account for about 80 percent of the total anthropogenic sources: coal-fired power plants, 33 percent; municipal waste incinerators, 18 percent; commercial and industrial boilers, 18 percent; and medical waste incinerators, 10 percent. The next step for EPA is to assess the need for enhanced research on health effects and on new pollution control technologies, community "right-to-know" approaches, and regulatory actions.

The results of the HAPs program have significantly mitigated concerns about HAPs emission from coal-fired generation and focused attention on but a few flue gas constituents. The results have the potential to make the forthcoming EPA regulations less strict, which could avoid unnecessary control costs and thus save consumers money on electricity bills.

Exhibit C-6
Status of Environmental Monitoring Plans for CCT Projects

Project and Participant	Status
CCT-I	
Development of the Coal Quality Expert (ABB Combustion Engineering, Inc., and CQ Inc.)	Completed 7/31/90
LIMB Demonstration Project Extension and Coolside Demonstration (The Babcock & Wilcox Company)	Completed 10/19/88
Advanced Cyclone Combustor with Internal Sulfur, Nitrogen, and Ash Control (Coal Tech Corporation)	Completed 9/22/87
Nucla CFB Demonstration Project (Colorado-Ute Electric Association, Inc.; now Tri-State Generation and Transmission Association, Inc.)	Completed 2/27/88
Enhancing the Use of Coals by Gas Reburning and Sorbent Injection (Energy and Environmental Research Corporation)	Completed 10/15/89 (Hennepin) Completed 11/15/89 (Lakeside)
Tidd PFBC Demonstration Project (The Ohio Power Company)	Completed 5/25/88
Advanced Coal Conversion Process Demonstration (Rosebud SynCoal Partnership)	Completed 4/7/92
JEA Large-Scale CFB Combustion Demonstration Project	Projected 6/01
CCT-II	
SNOX™ Flue Gas Cleaning Demonstration Project (ABB Environmental Systems)	Completed 10/31/91
Demonstration of Coal Reburning for Cyclone Boiler NO_x Control (The Babcock & Wilcox Company)	Completed 11/18/91
SO_x-NO_x-Rox Box™ Flue Gas Cleanup Demonstration Project (The Babcock & Wilcox Company)	Completed 12/31/91
Cement Kiln Flue Gas Recovery Scrubber (Passamaquoddy Tribe)	Completed 3/26/90
Advanced Flue Gas Desulfurization Demonstration Project (Pure Air on the Lake, L.P.)	Completed 1/31/91
Demonstration of Advanced Combustion Techniques for a Wall-Fired Boiler (Southern Company Services, Inc.)	Completed 9/14/90
Demonstration of Innovative Applications of Technology for the CT-121 FGD Process (Southern Company Services, Inc.)	Completed 12/18/90
Demonstration of Selective Catalytic Reduction Technology for the Control of NO_x Emissions from High-Sulfur-Coal-Fired Boilers (Southern Company Services, Inc.)	Completed 3/11/93
180-MWe Demonstration of Advanced Tangentially Fired Combustion Techniques for the Reduction of NO_x Emissions from Coal-Fired Boilers (Southern Company Services, Inc.)	Completed 12/27/90

Exhibit C-6 (continued)
Status of Environmental Monitoring Plans for CCT Projects

Project and Participant	Status
CCT-III	
Commercial-Scale Demonstration of the Liquid-Phase Methanol (LPMEOH™) Process (Air Products Liquid Phase Conversion Company, L.P.)	Completed 8/29/96
10-MW Demonstration of Gas Suspension Absorption (AirPol, Inc.)	Completed 10/2/92
Healy Clean Coal Project (Alaska Industrial Development and Export Authority)	Completed 4/11/97
Full-Scale Demonstration of Low-NO_x Cell Burner Retrofit (The Babcock & Wilcox Company)	Completed 8/9/91
Confined Zone Dispersion Flue Gas Desulfurization Demonstration (Bechtel Corporation)	Completed 6/12/91
Blast Furnace Granular-Coal Injection System Demonstration Project (Bethlehem Steel Corporation)	Completed 12/23/94
McIntosh Unit 4A PCFB Demonstration Project (City of Lakeland, Lakeland Electric)	Projected 8/01
ENCOAL® Mild Coal Gasification Project (ENCOAL Corporation)	Completed 5/29/92
Evaluation of Gas Reburning and Low-NO_x Burners on a Wall-Fired Boiler (Energy and Environmental Research Corporation)	Completed 7/26/90
LIFAC Sorbent Injection Desulfurization Demonstration Project (LIFAC–North America)	Completed 6/12/92
Integrated Dry NO_x/SO_2 Emissions Control System (Public Service Company of Colorado)	Completed 8/5/93
Tampa Electric Integrated Gasification Combined-Cycle Project (Tampa Electric Company)	Completed 5/96
Commercial Demonstration of NOXSO SO_2/ NO_x Removal Flue Gas Cleanup System (NOXSO Corporation)	To be determined
CCT-IV	
Micronized Coal Reburning Demonstration for NO_x Control (New York State Electric & Gas Corporation)	Completed 8/97
Milliken Clean Coal Technology Demonstration Project (New York State Electric & Gas Corporation)	Completed 12/1/94
Piñon Pine IGCC Power Project (Sierra Pacific Power Company)	Completed 10/31/96
Wabash River Coal Gasification Repowering Project (Wabash River Coal Gasification Repowering Project Joint Venture)	Completed 7/9/93
Pulse Combustor Design Qualification Test	To be determined
Self-Scrubbing Coal™: An Integrated Approach to Clean Air (Custom Coals International)	To be determined
CCT-V	
Clean Coal Diesel Demonstration Project (Arthur D. Little, Inc.)	Projected 2/99
Clean Power from Integrated Coal/Ore Reduction (CPICOR™) (CPICOR™ Management Company, L.L.C.)	Projected 9/02
Clean Energy Demonstration Project (Clean Energy Partners Limited Partnership)	To be determined
McIntosh Unit 4B Topped PCFB Demonstration Project (City of Lakeland, Lakeland Electric)	Projected 8/03

Exhibit C-7
CCT Projects Monitoring Hazardous Air Pollutants

Application Category	Participant	Project	Status
Advanced Electric Power Generation	Alaska Industrial Development and Export Authority	Healy Clean Coal Project	Planned
	Arthur D. Little, Inc.	Clean Coal Diesel Demonstration Project	Planned
	Clean Energy Partners Limited Partnership	Clean Energy Demonstration Project	Planned
	City of Lakeland, Lakeland Electric	McIntosh Unit 4B Topped PCFB Demonstration Project	Planned
	The Ohio Power Company	Tidd PFBC Demonstration Project	Completed
	Sierra Pacific Power Company	Piñon Pine IGCC Power Project	Planned
	Tampa Electric Company	Tampa Electric Integrated Gasification Combined-Cycle Project	In progress
	Wabash River Coal Gasification Repowering Project Joint Venture	Wabash River Coal Gasification Repowering Project	In progress
	JEA	Large Scale CFB Combustion Demonstration Project	Planned
Environmental Control Devices	ABB Environmental Systems	SNOX™ Flue Gas Cleaning Demonstration Project	Completed
	AirPol, Inc.	10-MWe Demonstration of Gas Suspension Absorption	Completed
	The Babcock & Wilcox Company	Demonstration of Coal Reburning for Cyclone Boiler NO_x Control	Completed
	The Babcock & Wilcox Company	SO_x-NO_x-Rox Box™ Flue Gas Cleanup Demonstration Project	Completed
	New York State Electric & Gas Corporation	Milliken Clean Coal Technology Demonstration Project	In progress
	Public Service Company of Colorado	Integrated Dry NO_x/SO_2 Emissions Control System	Completed
	Pure Air on the Lake, L.P.	Advanced Flue Gas Desulfurization Demonstration Project	Completed
	Southern Company Services, Inc.	Demonstration of Advanced Combustion Techniques for a Wall-Fired Boiler	Completed
	Southern Company Services, Inc.	Demonstration of Innovative Applications of Technology for the CT-121 FGD Process	Completed
	Southern Company Services, Inc.	180-MWe Demonstration of Advanced Tangentially Fired Combustion Techniques for the Reduction of NO_x Emissions from Coal-Fired Boilers	Completed
Coal Processing for Clean Fuels	ENCOAL Corporation	ENCOAL® Mild Coal Gasification Project	Completed
Industrial Applications	CPICOR™ Management Company, L.L.C.	Clean Power from Integrated Coal/Ore Reduction (CPICOR™)	Planned

Appendix D: CCT Project Contacts

Project Contacts

Listed below are contacts for obtaining further information about specific CCT Program demonstration projects. Listed are the name, title, phone number, fax number, mailing address, and e-mail address, if available, for the participant's contact person. In those instances where the project participant consists of more than one company, a partnership, or joint venture, the mailing address listed is that of the contact person. In addition, the names, phone numbers, and e-mail addresses for contact persons at DOE Headquarters and the Federal Energy Technology Center are provided.

Environmental Control Devices

SO_2 Control Technologies

10-MWe Demonstration of Gas Suspension Absorption

Participant:
AirPol, Inc.

Contacts:
Niels H. Kastrup
(281) 539-3400
(281) 539-3411 (fax)
nhk@flsmiljous.com

FLS Miljo, Inc.
100 Glenborough
Houston, TX 77067

Lawrence Saroff, DOE/HQ, (301) 903-9483
lawrence.saroff@hq.doe.gov
James U. Watts, FETC, (412) 892-5991
watts@fetc.doe.gov

Confined Zone Dispersion Flue Gas Desulfurization Demonstration

Participant:
Bechtel Corporation

Contacts:
Joseph T. Newman, Project Manager
(415) 768-1189
(415) 768-5420 (fax)

Bechtel Corporation
P.O. Box 193965
San Francisco, CA 94119-3965

Lawrence Saroff, DOE/HQ, (301) 903-9483
lawrence.saroff@hq.doe.gov
Robert M. Koanosky, FETC, (412) 892-4521
kornosky@fetc.doe.gov

LIFAC Sorbent Injection Desulfurization Demonstration Project

Participant:
LIFAC–North America

Contacts:
Jim Hervol, Project Manager
(412) 497-2235
(412) 497-2298 (fax)

ICF Kaiser Engineers, Inc.
Gateway View Plaza
1600 West Carson Street
Pittsburgh, PA 15219-1031

Lawrence Saroff, DOE/HQ, (301) 903-9483
lawrence.saroff@hq.doe.gov
James U. Watts, FETC, (412) 892-5991
watts@fetc.doe.gov

Advanced Flue Gas Desulfurization Demonstration Project

Participant:
Pure Air on the Lake, L.P.

Contacts:
Tim Roth
(610) 481-6257
(610) 481-5820 (fax)

Pure Air on the Lake, L.P.
c/o Air Products and Chemicals, Inc.
7201 Hamilton Boulevard
Allentown, PA 18195-1501

Lawrence Saroff, DOE/HQ, (301) 903-9483
lawrence.saroff@hq.doe.gov
James U. Watts, FETC, (412) 892-5991
watts@fetc.doe.gov

Demonstration of Innovative Applications of Technology for the CT-121 FGD Process

Participant:
Southern Company Services, Inc.

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NO_x Control Technologies

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Evaluation of Gas Reburning and Low-NO_x Burners on a Wall-Fired Boiler

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Demonstration of Selective Catalytic Reduction Technology for the Control of NO_x Emissions from High-Sulfur-Coal-Fired Boilers

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180-MWe Demonstration of Advanced Tangentially-Fired Combustion Techniques for the Reduction of NO_x Emissions from Coal-Fired Boilers

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Combined SO_2/NO_x Control Technologies

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Enhancing the Use of Coals by Gas Reburning and Sorbent Injection

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Commercial Demonstration of the NOXSO SO_2/ NO_x Removal Flue Gas Cleanup System

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Appendix E: Acronyms, Abbreviations, and Symbols

Acronyms, Abbreviations, and Symbols

°C	degrees Celsius
°F	degrees Fahrenheit
$	dollars (U.S.)
$/kw	dollars per kilowatt
$/ton	dollars per ton
%	percent
®	registered trademark
™	trademark
ABB CE	ABB Combustion Engineering, Inc.
ABB ES	ABB Environmental Systems
ACFB	atmospheric circulating fluidized-bed
ADL	Arthur D. Little, Inc.
AFBC	atmospheric fluidized-bed combustion
AFGD	advanced flue gas desulfurization
AIDEA	Alaska Industrial Development and Export Authority
AOFA	advanced overfire air
APF	advanced particulate filter
ASME	American Society of Mechanical Engineers
Ass'n.	Association
ATCF	after tax cash flows
atm	atmosphere(s)
avg.	average
BFGCI	blast furnace granular-coal injection
BG	British Gas
BG/L	British Gas/Lurgi
Btu	British thermal unit(s)
Btu/kWh	British thermal units per kilowatt-hour
B&W	The Babcock & Wilcox Company
CAAA	Clean Air Act Amendments of 1990
$CaCO_3$	calcium carbonate (calcitic limestone)
CaO	calcium oxide (lime)
$Ca(OH)_2$	calcium hydroxide (calcitic hydrated lime)
$Ca(OH)_2$•MgO	dolomitic hydrated lime
Ca/N	calcium/nitrogen
CAPI	Clean Air Power Initiative
Ca/S	calcium/sulfur
$CaSO_3$	calcium sulfite
$CaSO_4$	calcium sulfate
CCOFA	close-coupled overfire air
CCT	clean coal technology
CCT I	First CCT Program solicitation
CCT II	Second CCT Program solicitation
CCT III	Third CCT Program solicitation
CCT IV	Fourth CCT Program solicitation
CCT V	Fifth CCT Program solicitation
CCT Program	Clean Coal Technology Demonstration Program
CDL®	Coal-Derived Liquid®
CEQ	Council on Environmental Quality
CFB	circulating fluidized bed
C/H	carbon/hydrogen
CKD	cement kiln dust
CO	carbon monoxide
CO_2	carbon dioxide
COP	Conference of Parties
CT-121	Chiyoda Thoroughbred-121
CQE™	Coal Quality Expert™
CQIM™	Coal Quality Impact Model™
CX	categorical exclusion
CZD	confined zone dispersion
DER	discrete emissions reduction
DME	dimethyl ether
DOE	U.S. Department of Energy
DOE/HQ	U.S. Department of Energy Headquarters
EA	environmental assessment
EER	Energy and Environmental Research Corporation
EFCC	externally fired combined cycle
EIA	Energy Information Administration
EIS	environmental impact statement
EMP	environmental monitoring plan
EPA	U.S. Environmental Protection Agency
EPAct	Energy Policy Act of 1992
EPRI	Electric Power Research Institute
ESP	electrostatic precipitator
EWG	exempt wholesale generator
ext.	extension
FBC	fluidized-bed combustion

FCCC	Framework Convention on Climate Change
Fe_2S	pyritic sulfur
FERC	Federal Energy Regulatory Commission
FETC	Federal Energy Technology Center
FGD	flue gas desulfurization
FONSI	finding of no significant impact
FRP	fiberglass-reinforced plastic
ft, ft^2, ft^3	foot (feet), square feet, cubic feet
FY	fiscal year
gal.	gallon(s)
gal/ft^3	gallons per cubic feet
GB	gigabyte(s)
GE	General Electric
GHG	greenhouse gases
GNOCIS	Generic NO_x Control Intelligence System
gpm	gallons per minute
GR	gas reburning
GR–LNB	gas reburning and low-NO_x burner
GR–SI	gas reburning and sorbent injection
GSA	gas suspension absorption
GVEA	Golden Valley Electric Association
GW	gigawatt(s)
GWe	gigawatt(s)-electric
H_2S	hydrogen sulfide
H_2SO_4	sulfuric acid
HAP	hazardous air pollutant
HCl	hydrogen chloride
HF	hydrogen fluoride
HGPFS	hot gas particulate filter system
HHV	high heating value
hr.	hour(s)
HRSG	heat recovery steam generator
IEA	International Energy Agency
IGCC	integrated gasification combined cycle
in, in^2, in^3	inch(es), square inches, cubic inches
JEA	Jacksonville Electric Authority
JBR	Jet Bubbling Reactor®
KCl	potassium chloride
K_2SO_4	potassium sulfate
kW	kilowatt(s)
kWh	kilowatt-hour(s)
lb.	pound(s)
L/G	liqud to gas ratio
LHV	low heating value
LIMB	limestone injection multistage burner
LNB	low-NO_x burner
LNCB®	low-NO_x cell burner
LNCFS	Low-NO_x Concentric-Firing System
LOI	loss on ignition
LPMEOH™	Liquid phase methanol™
LRCWF	low-rank coal-water-fuel
LSFO	limestone forced oxidation
MASB	multi-annular swirl burner
MB	megabyte(s)
MCFC	molten carbonate fuel cell
$MgCO_3$	magnesium carbonate
MgO	magnesium oxide
Mhz	megahertz
mills/kWh	mills per kilowatt hour
min.	minute(s)
mo.	month(s)
MTCI	Manufacturing and Technology Conversion International
MTF	memorandum (memoranda)-to-file
MW	megawatt(s)
MWe	megawatt(s)-electric
MWt	megawatt(s)-thermal
N_2	atmospheric nitrogen
Na/Ca	sodium/calcium
Na_2/S	sodium/sulfur
NaOH	sodium hydroxide
Na_2CO_3	sodium carbonate
NAAQS	National Ambient Air Quality Standards
NEPA	National Environmental Policy Act
NH_3	ammonia
NO_2	nitrogen dioxide
NOPR	Notice of Proposed Rulemaking
NO_x	nitrogen oxides
NSPS	New Source Performance Standards
NTHM	net tons of hot metal
NTIS	National Technical Information Service
NYSEG	New York State Electric & Gas Corporation
OC&PS	Office of Coal & Power Systems
O&M	operating and maintenance
O_2	oxygen
OTAG	Ozone Transport Assessment Group
OTC	Ozone Transport Commission
PC	personal computer
PCAST	Presidential Committee of Advisors on Science and Technology
PCFB	pressurized circulating fluidized bed
PDF®	Process-Derived Fuel®
PEIA	programmatic environmental impact assessment
PEIS	programmatic environmental impact statement
PEOA™	Plant Emission Optimization Advisor™
PENELEC	Pennsylvania Electric Company

PEP	progress evaluation plan
PFBC	pressurized fluidized-bed combustion
PJBH	pulse jet baghouse
PM	particulate matter
PM_{10}	particulate matter less than 10 microns in diameter
$PM_{2.5}$	particulate matter less than 2.5 microns in diameter
PON	program opportunity notice
PRB	Powder River Basin
ppm	parts per million (mass)
ppmv	parts per million by volume
PSCC	Public Service Company of Colorado
PSD	Prevention of Significant Deterioration
psi	pound(s) per square inch
PUHCA	Public Utility Holding Company Act of 1935
PURPA	Public Utility Regulatory Policies Act of 1978
QF	qualifying facility
RAM	random access memory
R&D	research and development
RD&D	research, development, and demonstration
REA	Rural Electrification Administration
RP&L	Richmmond Power & Light
ROD	Record of Decision
rpm	revolutions per minute
RUS	Rural Utility Service
S	sulfur
SBIR	Small Business Innovation Research
scf	standard cubic feet
scfm	standard cubic feet per minute
SCR	selective catalytic reduction
SCS	Southern Company Services, Inc.
SFC	Synthetic Fuels Corporation
S-H-U	Saarberg-Hölter-Umwelttechnik
SI	sorbent injection
SIP	state implementation plan
SM	service mark
SNCR	selective noncatalytic reduction
SNRB™	SO_x-NO_x-Rox Box™
SO_2	sulfur dioxide
SO_3	sulfur trioxide
std ft^3	standard cubic feet
SOFA	separated overfire air
STTR	Small Business Technology Transfer Program
SVGA	super video graphics adapter
TAG™	Technical Assessment Guide™
TCLP	toxicity characteristics leaching procedure
TVA	Tennessee Valley Authority
UAF	University of Alaska, Fairbanks
UARG	Utility Air Regulatory Group
UBCL	unburned carbon
U.K.	United Kingdom
U.S.	United States
VFB	vibrating fluidized-bed
VOC	volatile organic compound
WC	water column
WES	wastewater evaporation system
WLFO	wet limestone, forced oxidation
wt.	weight
yr.	year(s)

State Abbreviations

States are abbreviated using two-letter postal codes.

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