Hydrogen Release from Simulated Sludge and Saltcake

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SUMMARY

Investigations into the nature and extent of hydrogen release from high level waste sludge and saltcake provide the following insights.

• Saltcake retains the majority of trapped gases during agitation events (including earthquakes).

• Of the nine tanks of concern from release of hydrogen during seismic events, three likely contain little trapped gas due to high thermal gradients in these tanks.

- Instrumentation of Tanks 7F and 13H to verify this conclusion is strongly recommended.

• The trapped gas in eight of the nine tanks of interest likely contain significantly less than 50% hydrogen.

- Additional testing is underway to confirm this conclusion.

• Sloshing of sludge and supernate in a vessel releases trapped gases.

-Material in the convective (sloshing) zone of the vessel releases nearly all trapped gas.

- Material in the impulsive zone (lower portion of the material that moves as a solid body) of the vessel releases little trapped gas.

• Sloshing will likely occur to some extent in all high level waste tanks that contain supernate and sludge during earthquakes. Current analyses suggest that the majority of this material will fluidize.

• Simplified theoretical models suggests that a lesser amount of fluidization will occur in tanks without a significant liquid layer.

INTRODUCTION

This report describes the results of the Savannah River Technology Center (SRTC) program to address bubble gas release potential as requested by Concentration, Storage and Transfer Engineering.¹ Researchers from the Waste Processing Technology Section (WPTS) and Immobilization Technology Section (ITS) contributed to the results presented.

Previously, personnel made measurements of the hydrogen concentrations in tank vapor spaces.^{2,3,4} These measurements demonstrated that hydrogen is released from the tank contents upon agitation. Previous laboratory work^{5,6} showed measurable quantities of hydrogen produced by radiolysis in tetraphenylborate slurries, sludge and saltcakes. Retention of hydrogen within High Level Waste tanks poses a potential safety concern.⁷ An analysis of the potential for exceeding the hydrogen flammability limit in the high level waste tanks was performed. This analysis made three primary assumptions: that sludge can contain 20 vol % trapped gas, that trapped gas consists of 50% hydrogen or less and that 50% of trapped gas releases during a seismic event.¹¹ Work has been performed to identify the validity of each of these assumptions. Weber et al. ¹⁴developed a method to estimate the volume of the trapped gas in high level waste tanks. Laboratory experiments provide estimates of the fraction of hydrogen in trapped gases and the amount of trapped gas released during a seismic event.^{8,9} This document reports on experiments designed to illuminate the extent of gas

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released from both sludge and salt matrices. These experiments are analyzed in relation to sudden agitation that occurs during an earthquake.

Extensive work performed at Pacific Northwest National Laboratory (PNNL) estimated the quantity of gases retained in settled solids. These results indicate that for yield strengths of approximately 10 Pa, the sludge studied could retain as much as 20% of their volume in gases.¹⁰ Those studies did not, however, indicate the quantity of gas released during agitation events and, in particular, during the design basis earthquake. This report describes experiments providing an experimental measure of gas bubble release during events similar to the design basis earthquake.

DISCUSSION

Tank Considerations

High Level Waste at the Savannah River Site generally exists in three forms, as saltcake, as sludge and as supernate. Generally speaking, all the high level waste tanks contain some quantity of supernate. However, the tanks can be divided into classes shown in Table 1.

Table 1. Classification of High Level Waste Tanks

Tanks with Sludge and Supernate	Tanks with Saltcake and Supernate
6F, 7F , 11H, 13H , 22,H 23H, <i>26F</i> <i>32H</i> , 35H , 39H, 40H , <i>51H</i> , 42H, 43H,	1F, 2F, 3F, 9H, 10H, 14H 19F, 25F, 27F, 28F, 29H 30H, 31H, 36H, 37H, 38H 41H, 44F, 45F, 46F
Tanks with Sludge, Saltcake and Supernate	Tanks with Supernate only
4F, 33F 34F, 47F	18F, 21H,24H
Tanks with Dried Sludge & Saltcake	
5F, 8F, 12H, 15H	

Hester evaluated these tanks to determine the potential impact of hydrogen release from a seismic event upon the lower flammability limit.¹¹ This analysis assumed the following.

- No appreciable trapped gas would exist in tanks with only supernate
 - (eliminating the lower right hand entry from Table 1 from consideration).
- No appreciable trapped gas released from tanks with saltcake
 - (eliminating the upper right hand entry from Table 1 from consideration).
- Sludge would contain no more than 20% volume fraction trapped gas.
- The retained gas would contain 50% hydrogen.
- 50% of trapped gas would release during a seismic event.
- Supernate does not trap appreciable amounts of gas.
- Sludge layers less than 18 inches in depth do not trap gas.

This analysis indicated that 5 of the tanks in Table 1 (shown in bold) could exceed the lower flammability limit during a seismic event.¹¹ An additional four tanks pose a concern if the operating fill limits are reached (shown in italics in Table 1).

These assumptions derived from observations of work performed at PNNL. Mahlman showed that for simple salt solutions containing more than 0.8 M NO_3 , hydrogen provides less than 50% of the

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Figure 1. Maximum Sludge Temperature for Various High Level Waste Tanks

gas produced by radiolysis due to decreases in hydrogen production and increases in oxygen production.¹² As mentioned above Gauglitz showed that slurries of varying strengths generally hold less than 20 vol % trapped gas. Further experience at Hanford indicated that gas release events generally liberate less than 50% of the trapped gas.¹⁷ Preliminary modeling of the release from high strength materials by PNNL researchers indicated that these materials (such as saltcake) would not likely release trapped gas.¹⁷

Volume Fraction Retained

More than 40% of Hanford tanks studied show less than 10% retained gas volume.¹³ This data suggests that many of the tanks of concern at SRS may contain significantly lower volumes of trapped gas than assumed in Hester's analysis. In determining the void fraction of trapped gas retained, PNNL researchers developed a methodology for translating level change data from High Level Waste tanks into estimates of the void fraction of trapped gas. Recently, Weber made similar measurements for one of the SRS High Level Waste tanks containing sludge (Tank 32H)¹⁴. These estimates indicate that little or no trapped gas exists in Tank 32H.¹⁴

This data indicates that at least one mechanism exists for the transport of hydrogen through the sludge in this tank. The most mechanism for such transport is through convective mixing of the interstitial fluid in the sludge layer. A number of the high level waste tanks of interest produce significant amounts of heat through radiolysis. If no convective heat transfer occurred in these tanks fairly high temperatures would result in these waste tanks. Figure 1 provides an estimate of the maximum temperature that could be reached in these tanks if no convection occurs. (Currently, the tanks are not being cooled and the measured sludge temperatures are near those shown on Figure 1.) Figure 1 indicates that Tanks 32H and 13H would experience very high thermal gradients. These thermal gradients would lead to convective heat transport which would also result in significant loss of hydrogen, thus providing a potential explanation for the low volume fraction trapped gas observed in Tank 32H. Also note that Tanks 7F, 8F, and 35H should also have significant convection, and thus may retain significantly less than 20% volume fraction trapped gas. Additional measurements of trapped gas using level change and associated vapor sampling would confirm the extent to which trapped gas is retained in these tanks.

Gas Composition



Figure 2. Estimated Volume% Hydrogen Produced by Radiolysis

Using the nitrate ion concentrations measured in various tanks of interest, existing correlations¹² provide a preliminary estimate of the concentration of trapped gas in these tanks. Figure 2 contains these estimates. Figure 2 indicates that hydrogen accounts for significantly less than 50% of the trapped gas for all cases except for Tank 51H. If one replaces the assumption of 50% hydrogen with the values presented in Figure 2, a significantly lower hydrogen concentration in the vapor results during a seismic event for most of the tanks of interest. Based on these assumptions (and the assumption of 20 vol % trapped gas and 50% release), only Tanks 7F and 13H would possibly exceed the lower flammability limit during a seismic event (see Figure 3). Furthermore, only 40H, 47F and 51H would exceed 50% of the LFL. To credit the lower hydrogen concentration in these tanks, future studies should confirm the hydrogen ratios in the presence of the more complex solution matrix present in the High Level Waste Tanks. In particular, the study should investigate the impact of nitrite ion and various organic compounds present in the tank farm. The presence of organic compounds such as dibutyl phosphate and oxalate will result in the oxidation of these organics and thus the net consumption of oxygen. Since oxygen is the predominant gaseous product of radiolysis of solution containing high nitrate concentrations, the reduction in oxygen production results in a higher hydrogen fraction in trapped gas. Of the tanks of interest from Table 1 (those in italics and bold), Tank 26F is most likely to contain quantities of organic species that may impact the ratio of hydrogen in that tank relative to other radiolysis gases.

Trapped Gas Release

Experimental Methodology

Testing focused on the release of trapped gas from simulated waste solutions under controlled agitation. These tests used four types of simulated waste solutions and two methods for introducing trapped gas bubbles (see Table 2). The two methods of introducing gas include irradiation and by reaction of peroxide. Irradiation (to between 6 and 8 Mrad of γ irradiation from a Co-60 source) of these samples produced primarily H₂ and O₂. Peroxide decomposes in mixtures of bentonite clay and sodium hydroxide to produce O₂. (Note: peroxide decomposition in simulated sludge occurs too quickly for practical use.) These tests used about 4 mL of 30 wt % hydrogen peroxide per mL of solution. Previous work at Pacific Northwest National Laboratory indicated that the rheological

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Figure 3. Estimated Vapor Space

properties of 10 to 14 wt % bentonite clay mixtures approximate those of SRS sludge. Use of bentonite clay facilitates the development of proposed future larger-scale tests that can not utilize the Co-60 source.

Figure 4 describes the testing protocol used for those tests using irradiation for the production of trapped gases. When peroxide provided the trapped gas production, the tests used liquid level change to determine the quantity of trapped gas released.

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As received sludge simulant contain approximately 14 wt % solids.¹⁵ Concentrated sludge -- obtained by centrifuging as received sludge to achieve a 50 vol % reduction -- contains approximately 28 wt % solids. Note that the concentrated sludge would likely be more representative of settled sludge in the tank farm and the as received sludge would likely be more representative of washed sludge. However, since limited rheological data is available related to the contents of these tanks, correlations between the observed experimental results and anticipated tank results should be made carefully. It is likely that sludges in the tank farm span the behaviors observed for concentrated and as received sludge. The bentonite clay samples contained 11 to 12 wt % solids in water. Saltcake was prepared by evaporating a concentrated salt solution and cooling to room temperature.

Most of the tests in Table 2 used a 4 cm diameter vessel containing 50 mL of the mixture. This provided an aspect (i.e., depth-to-diameter) ratio of ~ 1 . Two additional tests used a larger vessel (~ 15 cm in diameter). These tests used an approximately 12 wt % bentonite slurry. The test vessel contained 5 and 10 cm of slurry for these two tests, yielding aspect ratios of 0.33 and 0.66. These

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frequencies and amplitudes used).

Table 2. Number of samples prepared for each test method.

	As Received	Concentrated	Bentonite Clay	Prepared
	Sludge	Sludge		Saltcake
Irradiation	10	2	None	5
Peroxide	none	None •	5	None

Each test used a fixed stroke length displacement in one direction such that the location of the sample (x) can be written as

Thus, these conditions provided the maximum response to the variable of interest (including

$$x = \frac{A}{2}\sin(f\pi t)$$

where A represents the stroke length (cm), f corresponds to the frequency (Hz), and t is time (s). The velocity (v) is:

$$v = \frac{dx}{dt} = 2f\pi \frac{A}{2}\cos(2f\pi t)$$

and the acceleration (a) is:

$$a = \frac{dv}{dt} = \frac{d^2x}{dt^2} = -4(f\pi)^2 \frac{A}{2}\sin(2f\pi t)$$

Thus, as the frequency increases, the acceleration – and thus the force acting on the sample—increased dramatically.

Experimental Results

Saltcake

Table 2 states that 5 tests investigated the impact of agitation on the release of trapped gas from saltcake. Initially, these samples were agitated in a controlled fashion. Analyses of these samples did not indicate any release of hydrogen. Additional strong agitation of this sample also provided less than detectable concentrations of hydrogen release. These results support the assumption that limited hydrogen will release from saltcake during a seismic event. The presence of layers of fluid sandwiched between salt cake layers was not addressed in this analysis.

Sludge

Tests performed using the sludge/hydrogen system indicated that the changes of the agitation frequencies affected each sample identically (see Figure 5). The system released a greater percentage of the trapped gas as the agitation frequency increased. Also note that as the agitation frequency

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increased, the amount of material in motion (i.e., sloshing) in the vessel increased. These tests used sludge simulants with relatively low yield strengths.

Additional tests using concentrated sludge provided significantly different results. The samples did not release measurable quantities of trapped gas when agitated, even at 4 Hz. The sludge sample did release measurable trapped gas when vigorously shaken by hand (see Figure 5). In Figure 5, the data point shown at 4.5 Hz represents shaken by hand, but not specifically at 4.5 Hz. These results suggest that more concentrated sludge samples (such as would be present near the bottom of a high level waste tank) would be less susceptible to release, while more dilute sludge (as would be present near the top of the sludge layer) would be more susceptible. It is likely that sludges in the tank farm span the behaviors observed for concentrated and as received sludge.

Figure 5. Release vs frequency



<u>Clay</u>

Figure 5 indicates relatively sharp dependence of trapped gas release on the amount of energy applied. Also, the amount released depends on strength of the retaining media. Note that for the clay samples, the amount of trapped gas released was determined by measuring the level before introduction of trapped gas, after introduction of trapped gas and after agitation.

Comparison of the unconcentrated and concentrated sludge samples readily shows the difference. At identical accelerations, the thicker – by 2X solids content – material produced completely different amounts of released trapped gas. The data suggest that fluidization of the material (and thus release) depends on a relationship between the force applied to the material and the strength of the material. In one case, the level after agitation was lower than prior to introduction of trapped gas. This suggests that a small amount of trapped gas existed in the system prior to testing and that this gas was released during agitation.

The experiments also studied release from larger (i.e., 15 cm diameter) vessels. In contrast to the work with smaller vessels, these tests examined a scan of both amplitude and frequency. At low frequency and amplitude, the material in the vessel behaved as a solid mass (see Figure 6A). At

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slightly increased frequency and amplitude, fluidization of the material occurred near the edges of the vessel (see Figure 6B). As energy input increased, this fluidization propagated through the material until, with enough energy supplied, the entire material fluidized (see Figure 6C and 6D). The tests proved that only the sloshing regions released the trapped gas. Other literature refers to the sloshing material as convective layers.¹⁶ The tests also examined effect of the agitation frequency on the depth of the convective layer. As the frequency increased, the convective layer expanded in depth. This expansion in the convective layer directly corresponded to an increase in the amount of gas released.



Computer Simulations

Researchers at PNNL developed a highly refined analytical model of the behavior of this material.¹⁷ However, it is insightful to first consider a highly simplified interpretation of the behavior of this material. Consider the material as a solid body moving horizontally in one direction at a given acceleration. Neglecting any elasticity of the material, the force acting on the material is simply the product of the mass and acceleration. If one considers a single element of the material, (with cross

section of 1 cm^2) the force acting on the material is simply the product of the acceleration and the column length (see Figure 6A). Thus, it is possible to provide a very crude estimate of the maximum force (and pressure) generated by the acceleration of the material. If this pressure exceeds the yield strength of the material, one may anticipate yielding (and thus localized fluidization) of the material. Figure 7 provides this rough estimate of the lateral accelerations overcoming the yield strength of these materials.rs complicates this analysis and has not been addressed herein. These results suggest that more concentrated sludge samples (such as would be present near the bottom of the tank) would be less susceptible to fluidization.

Modeling results from Reid and Deibler¹⁷ and Wassgren (see Appendix A) estimate that fluidization of the material will occur only near the surface of the tank. While neither of these models provide a rigorous description of the material behavior after the translation to fluid material, they do suggest that when no overlaying liquid exists, material of moderate strength will likely fluidize only near the surface of the tank during a seismic event. Verification that this behavior for tanks containing little or no liquid layer requires extensive data on the physical properties of these materials including a measure of the shear/strain relationship. As noted above, fluidization of weak material will occur. The degree of fluidization that occurs will vary in inverse proportion to the strength of the material. Thus, use of either of these models requires that tanks contain both a small amount of free liquid (not generally true of SRS tanks containing sludge) and thorough understanding of the material properties of the sludge (also generally lacking for SRS High Level Waste).

When the work of Reid and Deibler and of Wassgen analyzed the system containing a significant free liquid layer, they predicted fluidization of the majority of the sludge in the tank. While laboratory testing did not study this phenomenon, such behavior is expected to occur to a limited extent in the High Level Waste Tanks. Due to the ability to store energy in the free liquid layer, more energy can be transfered to the sludge when a free liquid layer exists. However, again, neither of these two models adequately describes the transition from solid to fluid behavior. If a more complete model proves desirable for program needs, additional refinement would focus on more accurately describe this transition. However, the development of such models likely represents a fairly extensive effort.

CONCLUSIONS

Hester's analysis of High Level Waste tanks identified nine tanks as most vulnerable to release of hydrogen during a seismic event in sufficient quantities to pose a flammability hazard. Laboratory testing of saltcake confirms the assumption that tanks containing only saltcake will not release significant quantities of trapped gas even when exposed to relatively large accelerations. Testing with simulated sludge with rheological properties typical of High Level Waste supports the contention that the solids retain no more than 20 vol % of trapped gases.¹⁰ In current analyses, sloshing of supernate over sludge results in fluidization and the release of trapped gas. Less fluidization occurs in tanks without a significant liquid layer. Calculations based on existing radiolysis studies suggests that the assumption of 50% hydrogen in the trapped gas appears overly conservative for all but one of the nine tanks, although additional testing in progress more rigorously evaluates this assumption.

Parallel work By Weber et al. and Bollinger and Hester suggest low volumes of trapped gas in Tank 32H. Calculations within show that such low retention may result from good transport of the gas due to thermally induced convection. Additional vapor sampling, and use of installed humidity and pressure monitoring equipment as deployed for Tank 32H would further support this contention. Of the nine identified tanks, Tanks 7F and 13H most likely benefit from this mixing. Efforts should

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focus on determining the quantity of retained gas. Without credit for lower gas retention, these two tanks might exceed the flammability limit of hydrogen during a seismic event.

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