

Spore forming bacteria
emerging and re-emerging issues

Summer Meeting 2005

**Thermal inactivation of
Alicyclobacillus spores
in fruit product processing**

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Brighton 4th – 7th July 2005

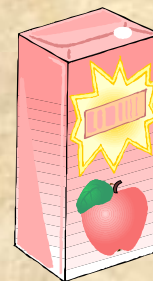
Characteristics

Alicyclobacillus acidoterrestris

- ◆ non-pathogenic
- ◆ spore-forming bacterium
- ◆ thermoacidophilic



found in
commercial pasteurized
fruit juices



Historical background

Alicyclobacillus acidoterrestris

in the 1980s ...

fruit juice industry faced a serious problem !!

consumers complained about spoilage juices

before shelf life had expired



off flavor
loss of color
no gas production

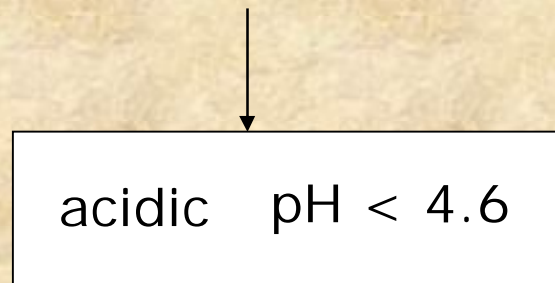


only a **spore former** could survive a thermal treatment in the pasteurization range

it had to be **acidophilic** to grow in acid juices

Design of the pasteurization processes

Fruit products



juices, nectars, concentrates of purées

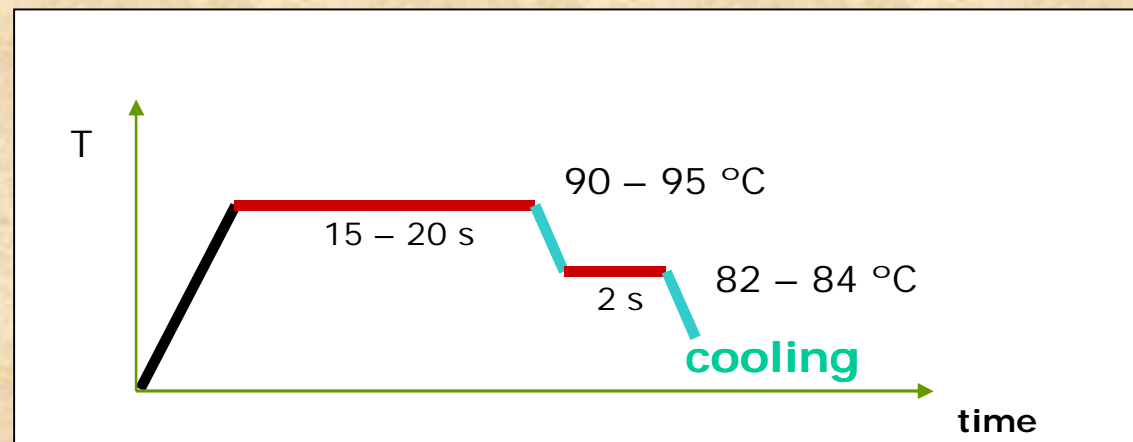
~~*Clostridium botulinum*~~

yeasts

molds

nonspore-forming bacteria

Pasteurization



adequate for stabilisation at ambient temperature

Design of the pasteurization processes

Fruit products

juices, nectars, concentrates of purées

What was happening

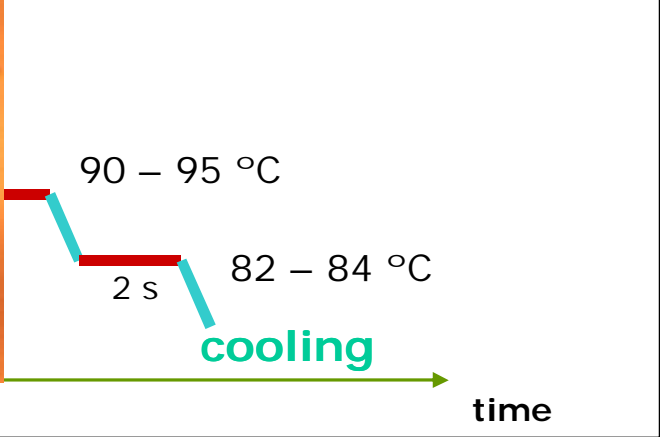
acidic pH < 4.6

Clostridium botulinum

forming bacteria



Pasteurization



adequate for stabilisation at ambient temperature

Design of the pasteurization processes

What was happening



Historical background

Alicyclobacillus acidoterrestris

1984 The microbial growth was isolated and identified as a **new type of spoilage bacterium**

First studies in aseptically packaged apple juice

(Cerny et al.)

1987 The species was first named as ***Bacillus acidoterrestris***

(Deinhard et al.)

1992 Reclassified as a new genus Alicyclobacillus, becoming ...

Alicyclobacillus acidoterrestris

(Wisotzkey et al.)

Design and optimization of pasteurization processes

Pasteurization

... should inactivate microorganisms' vegetative cells



bacteria
yeasts
molds

safety

and enzymes



quality

prevent the degradation of the original **organoleptic** and **nutritive** fruit characteristics

Design and optimization of pasteurization processes

however ...

thermal processes affect negatively quality factors

process design



Design and optimization of pasteurization processes

Pasteurization

acidic foods



inactivation of non-pathogenic microorganisms
and enzymes



non-acidic foods



inactivation of pathogenic microorganisms

Pasteurization methods

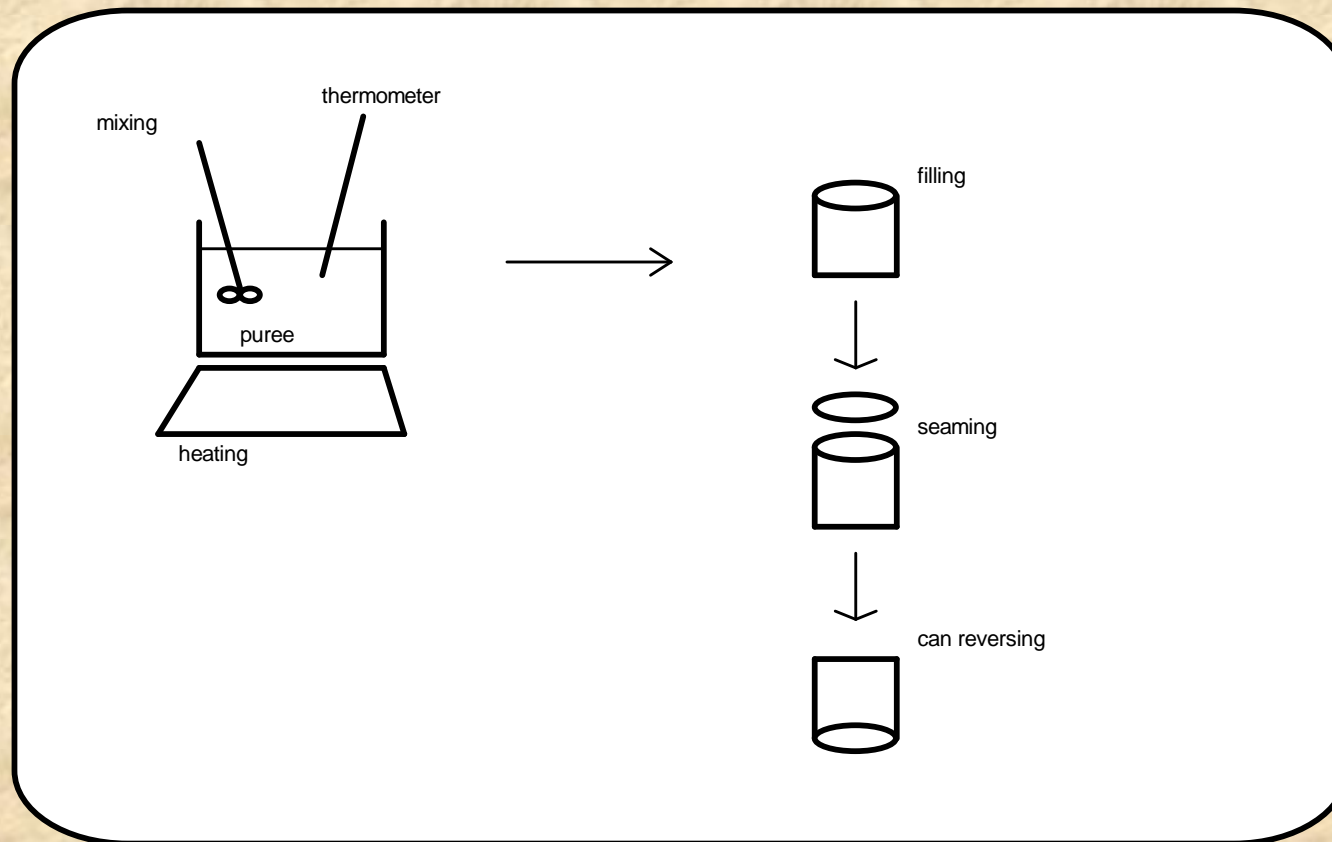
... applied to several fruit products

- hot filling
- aseptic process
- traditional canning

temperatures < 100 °C

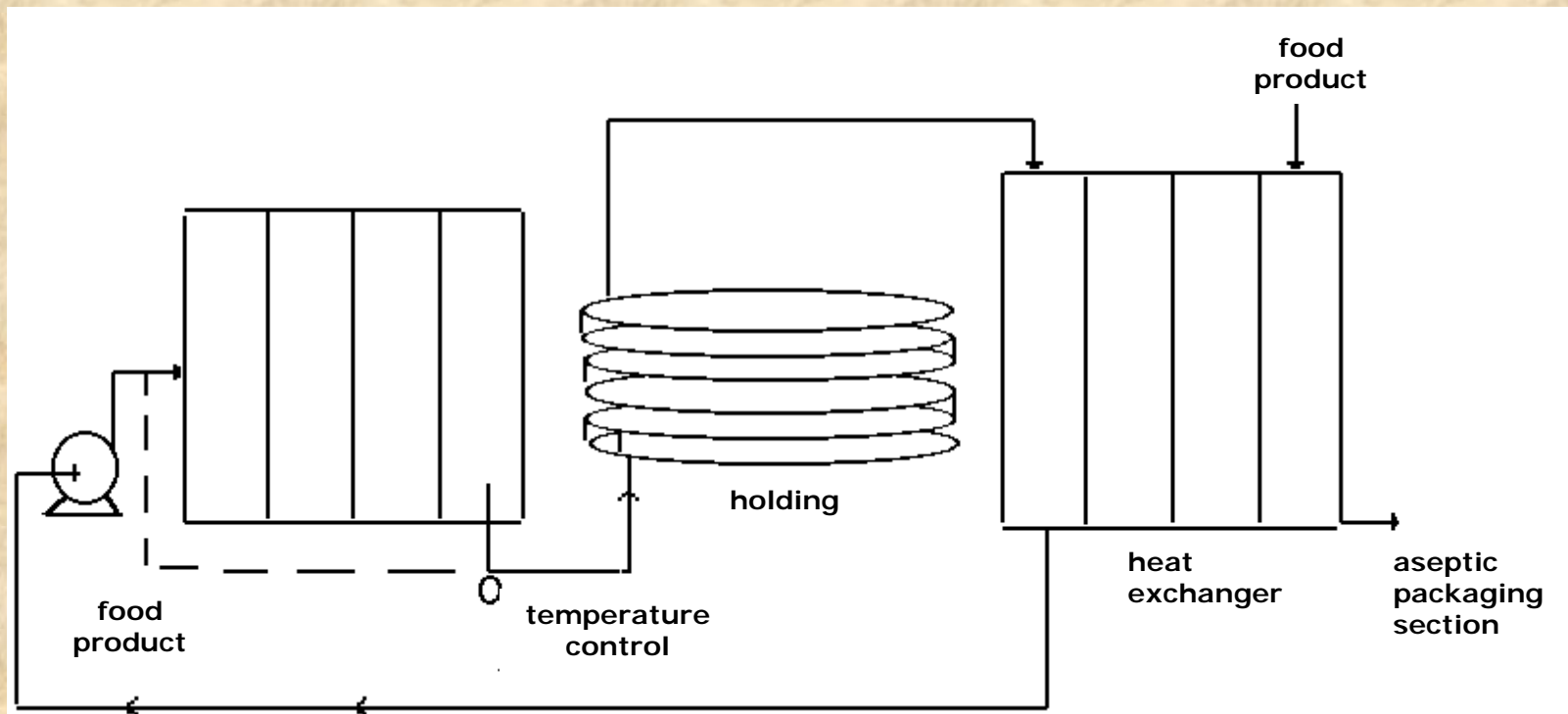
Design and optimization of pasteurization processes

- **hot filling**



Design and optimization of pasteurization processes

- aseptic process



Design and optimization of pasteurization processes

- aseptic process



Design and optimization of pasteurization processes

- **traditional canning**



Design and optimization of pasteurization processes

Target

... for shelf-stable high acidic fruit products

not very clear !

- Target **microorganisms/enzymes** and its inactivation requirements are not defined or vary with product
- No regulation available – depends usually on industrial experience

time / temperature ?

Alicyclobacillus acidoterrestris spores as pasteurization target

in 2000

establishment of a new pasteurization criterion for
shelf-stable high-acidic fruit products



Alicyclobacillus acidoterrestris spores

Filipa Silva (2000) **Ph.D. thesis** developed in Escola Superior de Biotecnologia
Universidade Católica Portuguesa, Portugal.

Research project:

***Multidisciplinary Study of the Transformation of Amazonian Fruits for their Commercial
Valorization Aiming at the Development of Local Rural Communities***

EU (DGXII) - program STD3
Portugal, Belgium, France and Brazil

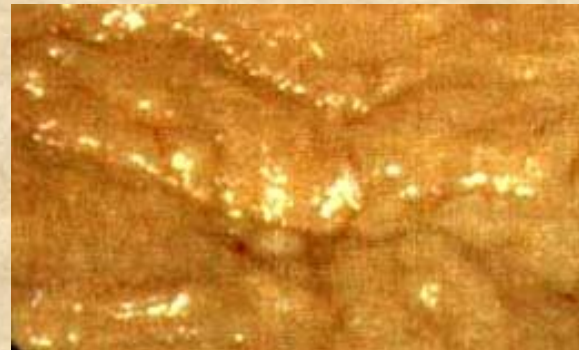
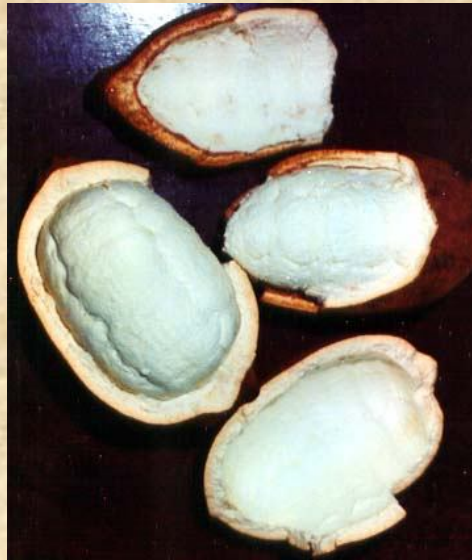
Alicyclobacillus acidoterrestris spores as pasteurization target



Cupuaçu

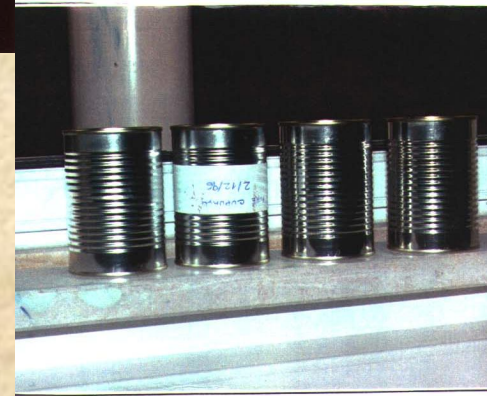
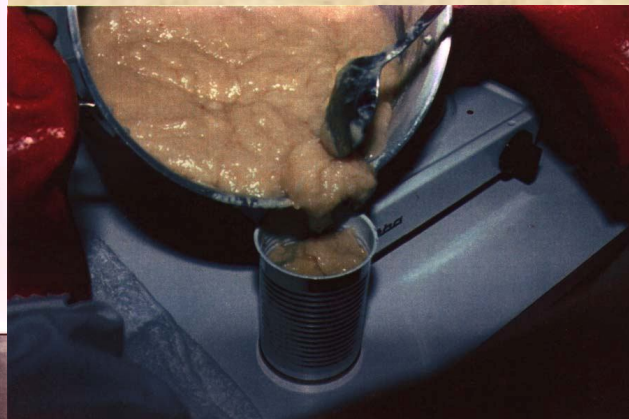
Theobroma grandiflorum

Design and optimization of pasteurization processes



Design and optimization of pasteurization processes

- hot filling



Design and optimization of pasteurization processes

pasteurization conditions for cupuaçu pulp

treatment	heating time (min)	holding time (min)	holding temperature (°C)
hot-filling	8.0	15	70
	8.2	10	75
	10.3	5	80
	11.3	2	85
	13.8	0	87
isothermal pasteurization conditions	3.7	1.3	70
	3.7	1.3	90



thermostatic water baths of TDT cans filled with cupuaçu pulp

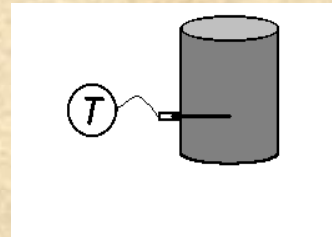
Design and optimization of pasteurization processes

pasteurized cupuaçu pulp

evaluation of the process



at the coldest point



estimation of
Alicyclobacillus acidoterrestris spores load

Design and optimization of pasteurization processes

How was it achieved ????

$$\frac{N}{N_0} = 10^{\left(\frac{-1}{D_{T_{\text{ref}}}} \int_0^{\text{PT}} 10^{\frac{T - T_{\text{ref}}}{z}} dt \right)}$$

function of time

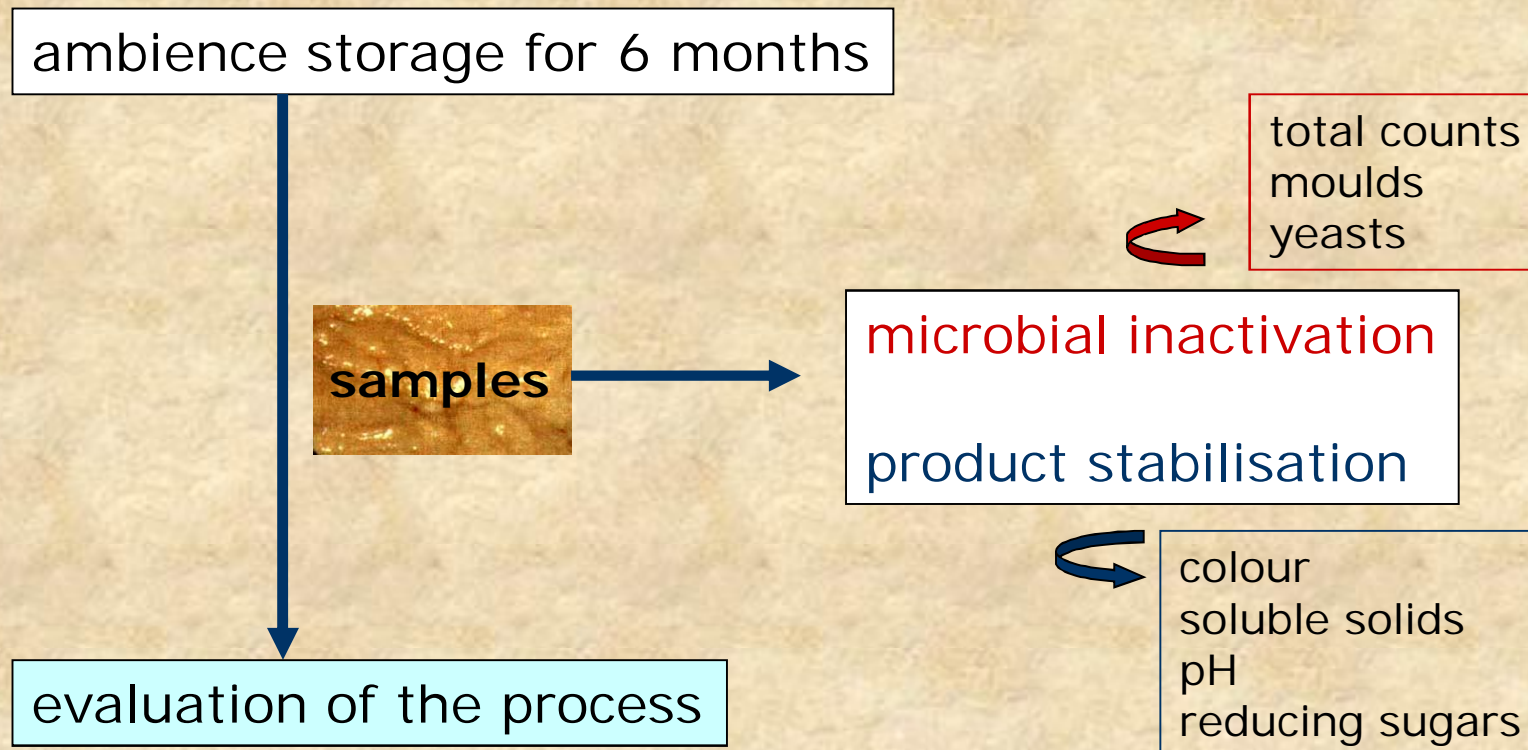
estimated parameters

D decimal reduction time
z- value

N number of viable spore cells
N₀ number of initial viable spore cells
T temperature
T_{ref} reference temperature
PT total process time

Design and optimization of pasteurization processes

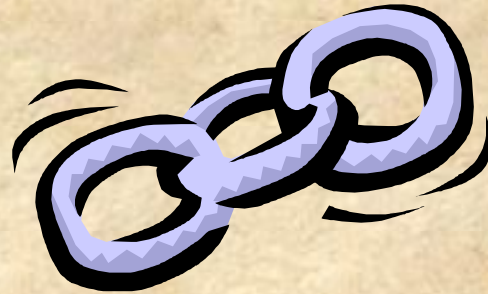
pasteurized cupuaçu pulp



The role of mathematical modelling

**predictive
microbiology**

microbiology



mathematics

statistics

The role of mathematical modelling

Predictive microbiology

The use of **mathematical models** in the description of **microbial responses** to environmental stressing factors

is gaining considerable importance in the food processing domain, particularly in the **design** of **efficient** and **safe inactivation treatments**

The role of mathematical modelling

objective

precise and accurate description of observations

model adequacy

quality of model parameters



The role of mathematical modelling

advantages

- **knowledge of the process**
- **process effect on product**
- **control of process variables**

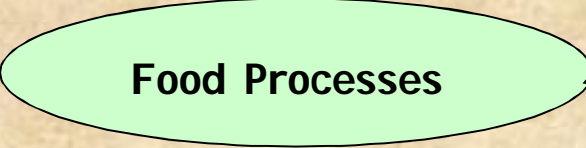
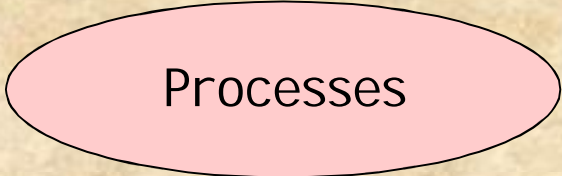
The role of mathematical modelling

Transport Phenomena

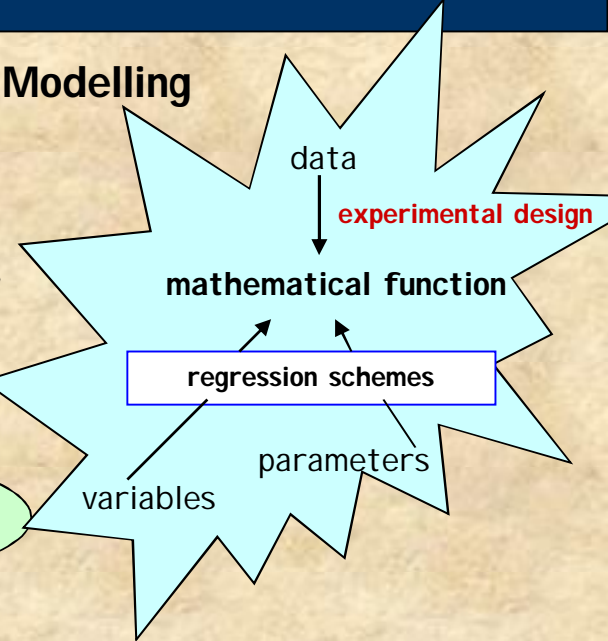
- heat
- mass
- *momentum*

Reaction kinetics

Properties



Modelling



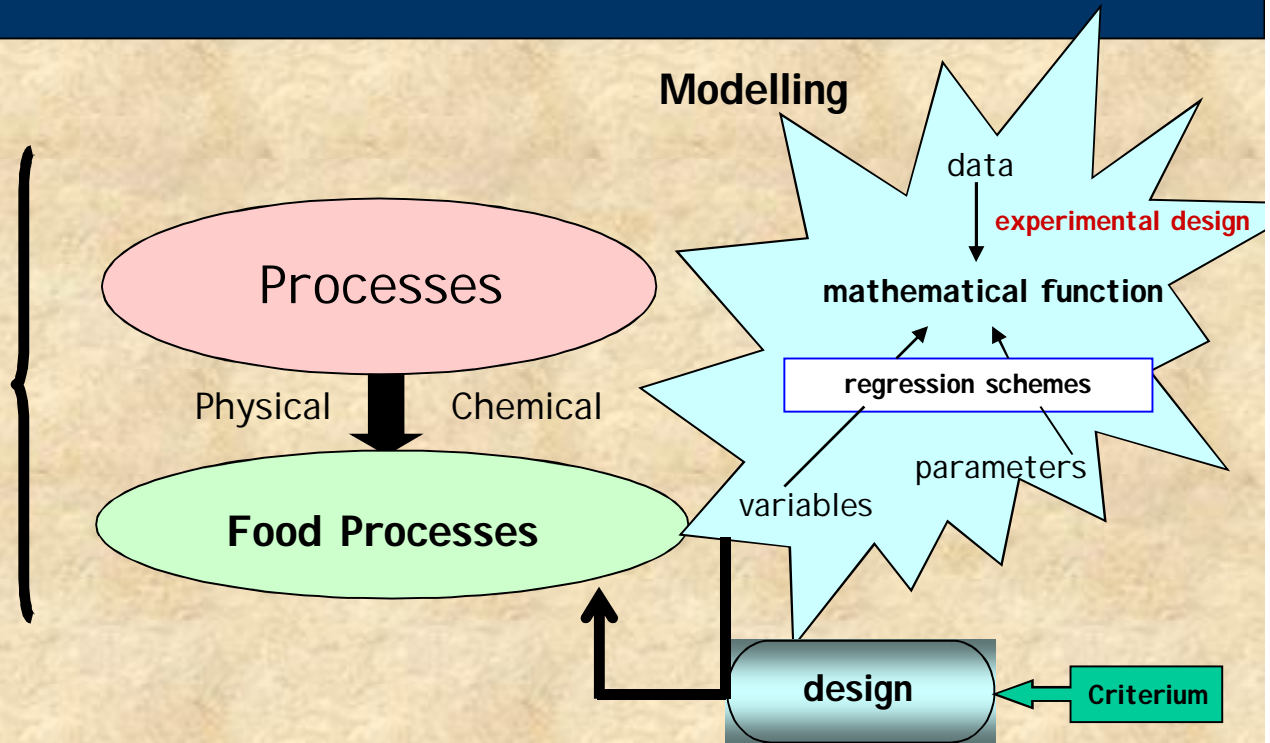
The role of mathematical modelling

Transport Phenomena

- heat
- mass
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Reaction kinetics

Properties



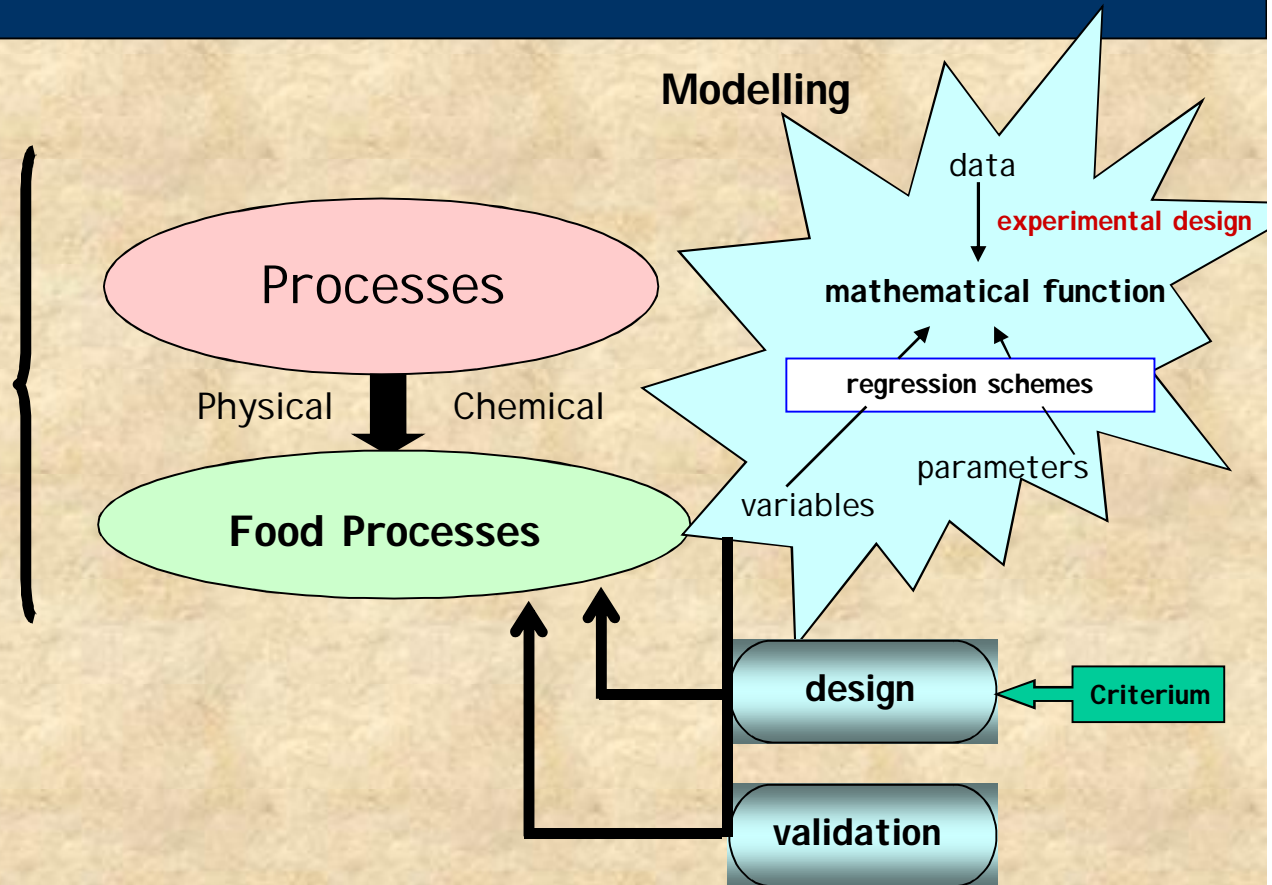
The role of mathematical modelling

Transport Phenomena

- heat
- mass
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Reaction kinetics

Properties



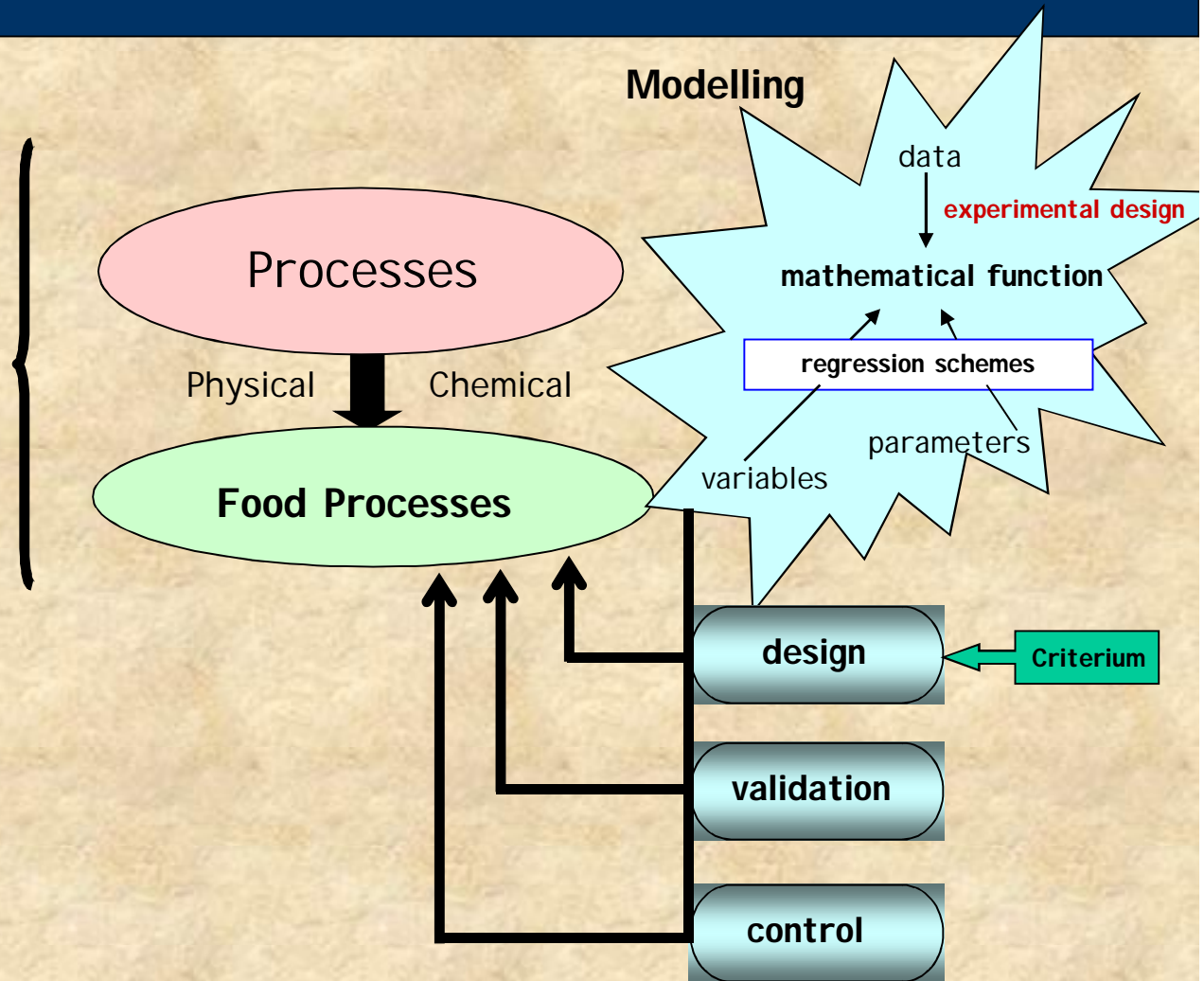
The role of mathematical modelling

Transport Phenomena

- heat
- mass
- *momentum*

Reaction kinetics

Properties



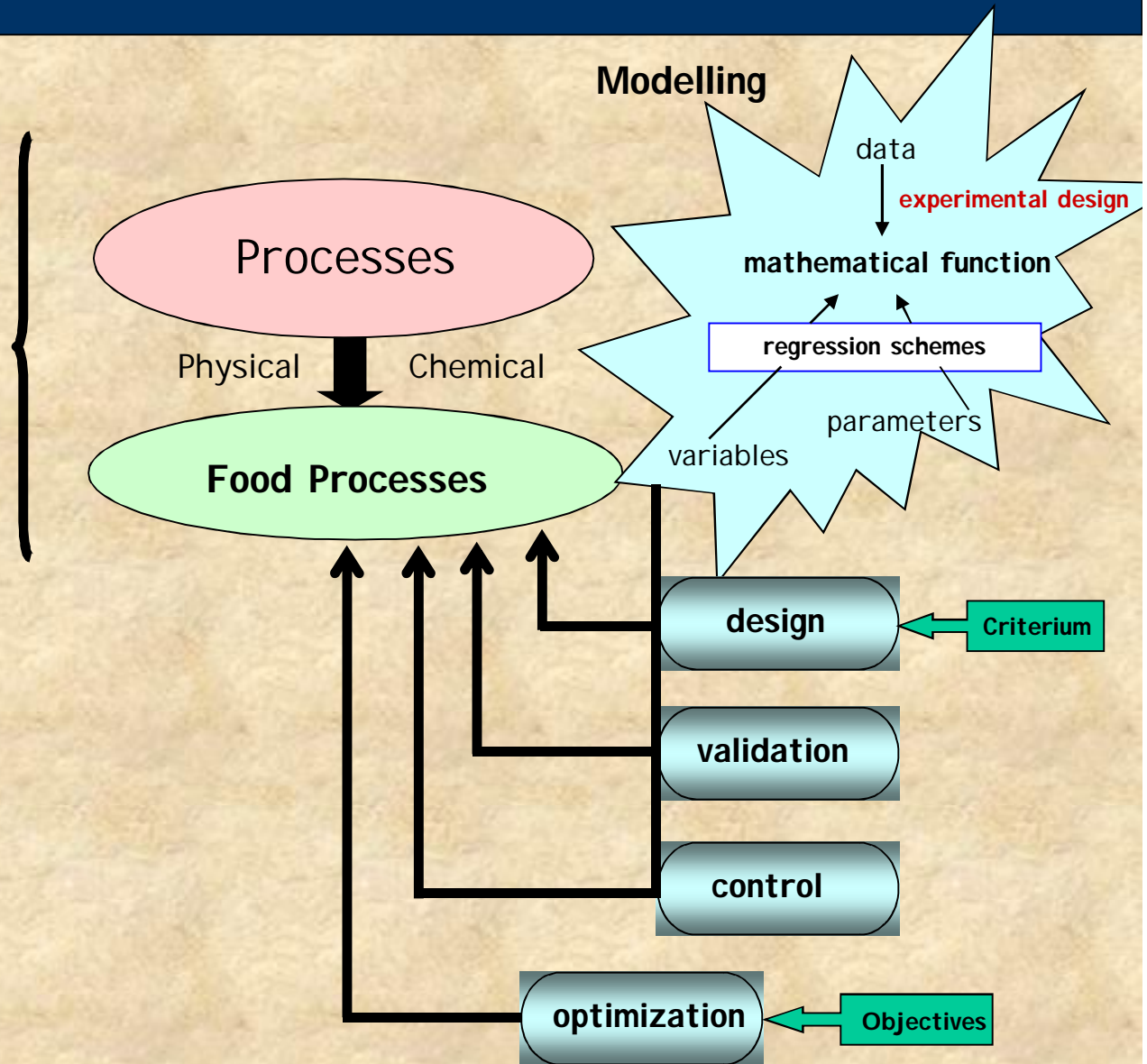
The role of mathematical modelling

Transport Phenomena

- heat
- mass
- *momentum*

Reaction kinetics

Properties



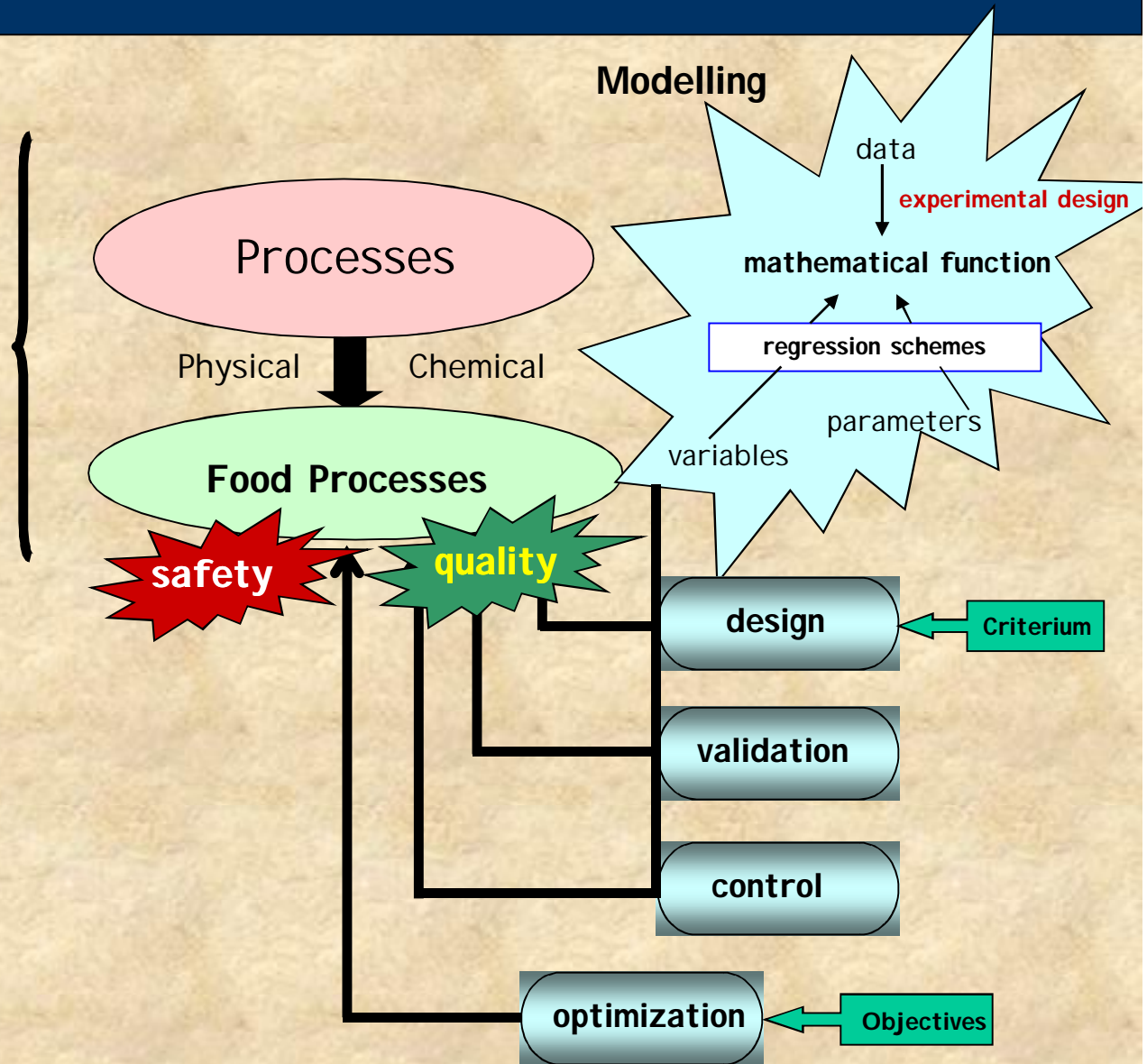
The role of mathematical modelling

Transport Phenomena

- heat
- mass
- *momentum*

Reaction kinetics

Properties



The role of mathematical modelling

application

- prediction / simulation
- development of efficient inactivation processes



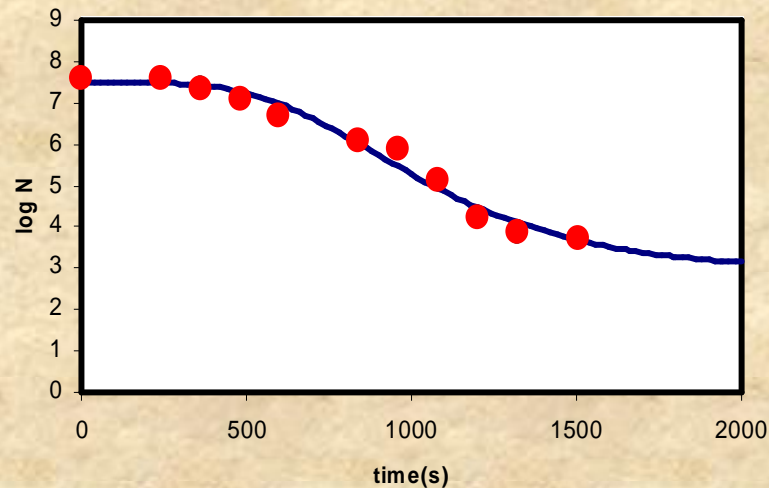
contribution to **safety**

Predictive microbiology

inactivation

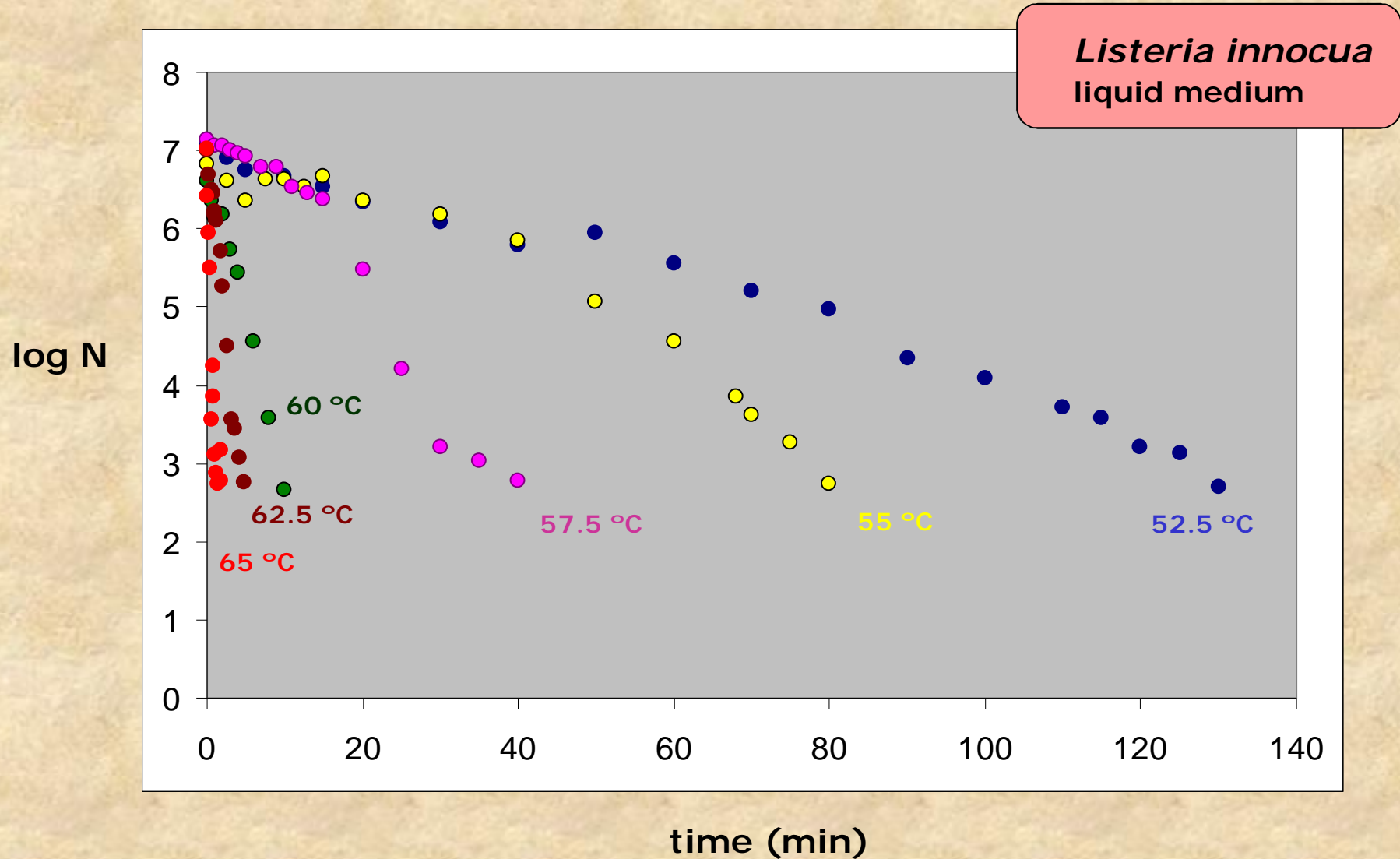


sigmoidal behaviour



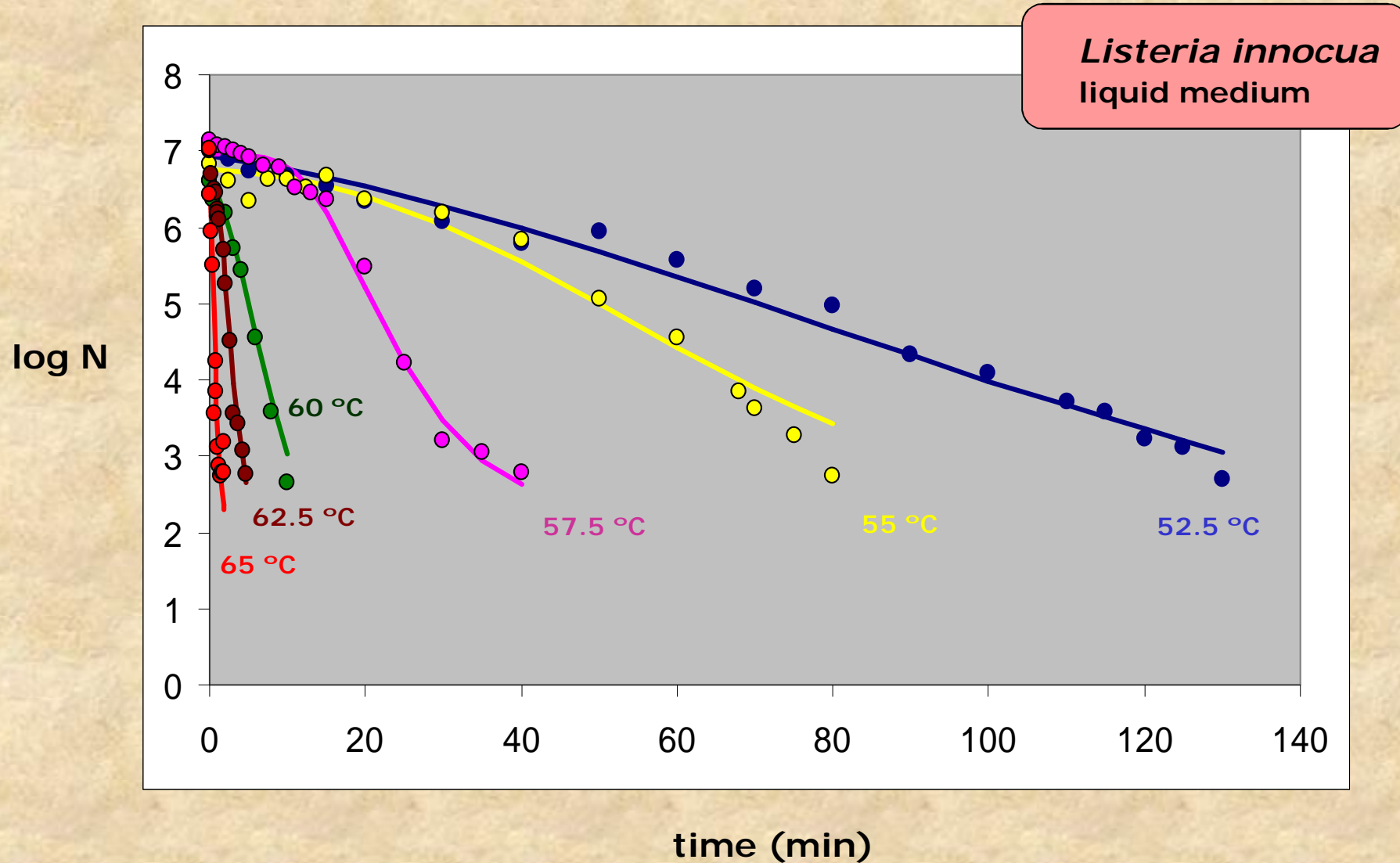
presence of aggregated microorganisms or sub populations
more **heat** (or other **stress factor**) **resistant**

Examples



Miller (2004)

Examples



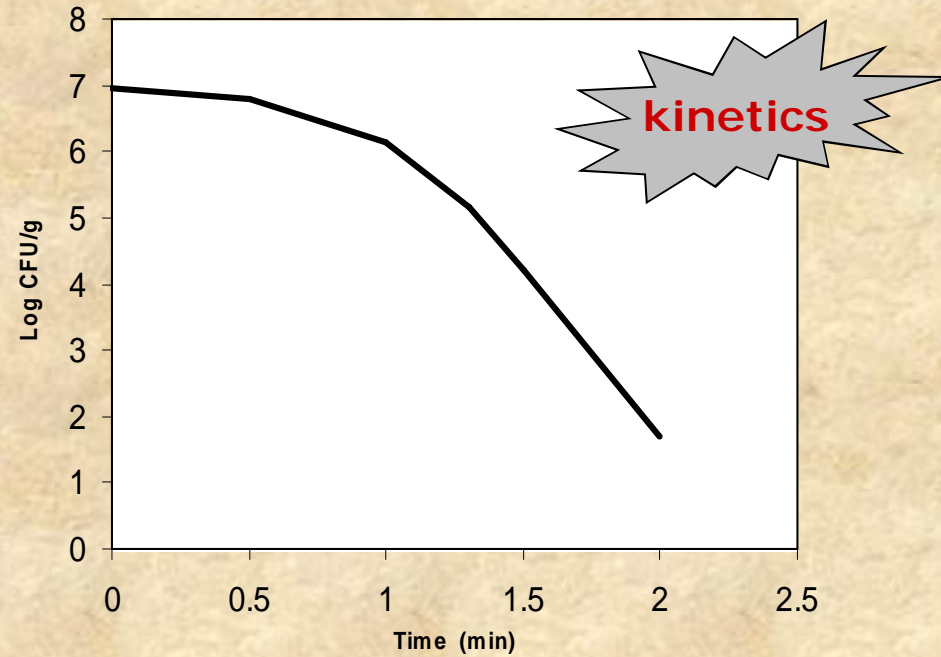
Miller (2004)

Mathematical models

❖ primary

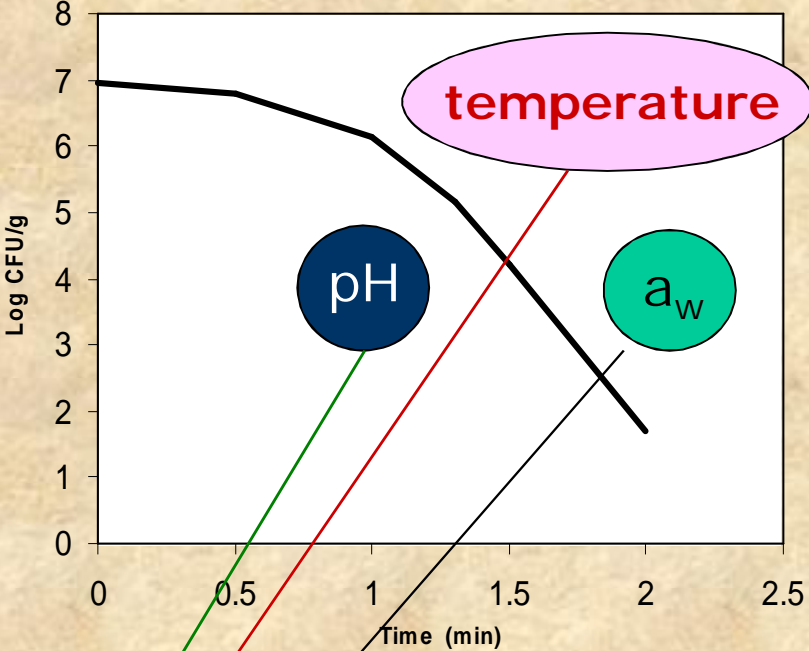


parameters



Mathematical models

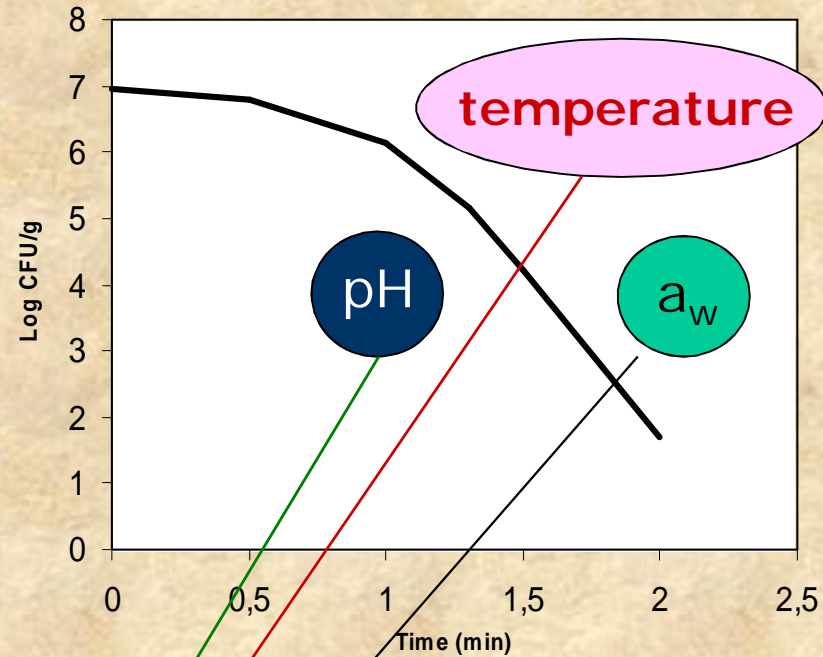
❖ primary



❖ secondary parameters

Mathematical models

❖ primary

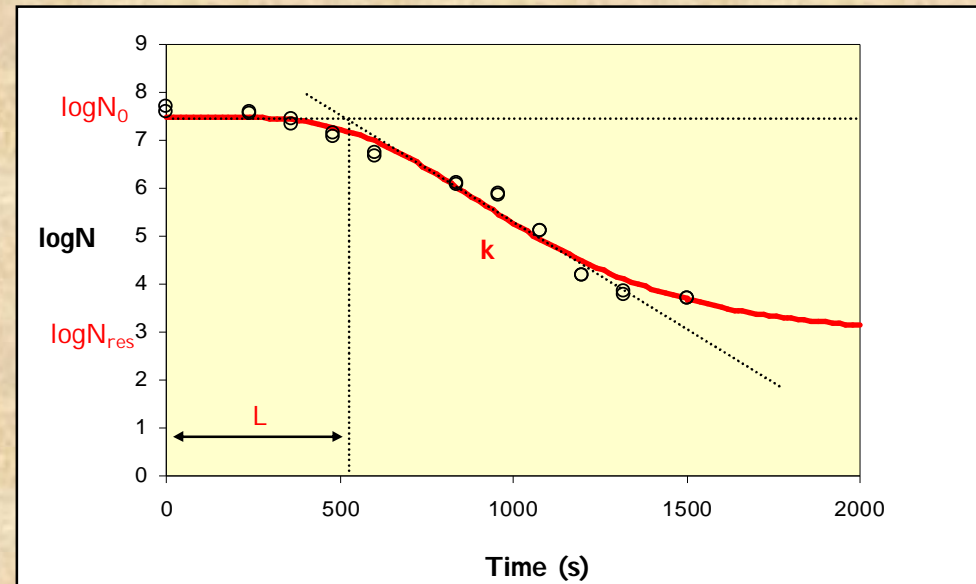


❖ secondary
parameters

❖ tertiary - integration of the previous models - software

Inactivation models

❖ primary



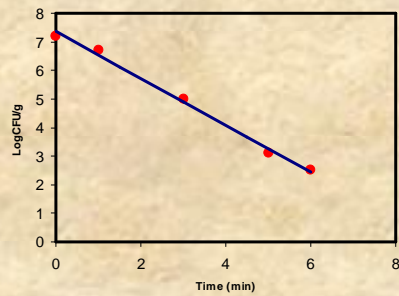
- N_0 number of initial viable spore cells
- N_{res} number of residual spore cells
- k maximum inactivation rate
- L lag or shoulder

empirical

fundamental

Inactivation models

❖ primary



$$N = N_0 \exp(-kt)$$



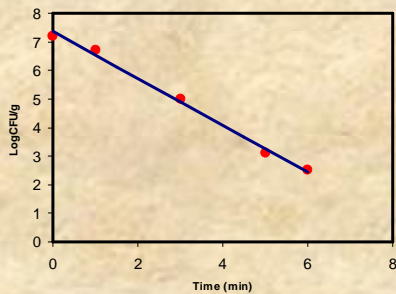
$$\log N = \log N_0 - \frac{t}{D}$$

First order

D – decimal reduction time

Inactivation models

❖ primary



$$N = N_0 \exp(-kt)$$



$$\log N = \log N_0 - \frac{t}{D}$$

First order

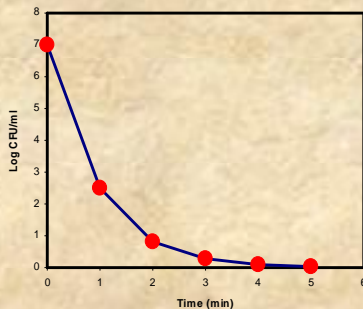
D – decimal reduction time

$$\frac{N}{N_0} = F_1 \exp(-k_1 t) + (1 - F_1) \exp(-k_2 t)$$

Cerf
(1977)

biphasic

F_1 – fraction of inactivated microorganisms
 k_1 e k_2 – kinetic constants

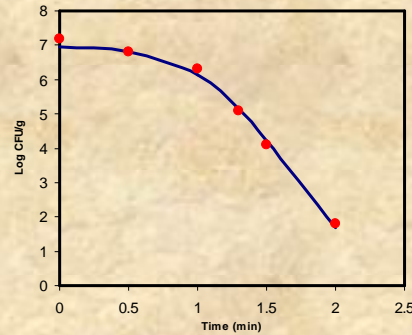


$$\log \frac{N}{N_0} = \log \left(\frac{2F_1}{1 + \exp(k_1 t)} + \frac{2(1 - F_1)}{1 + \exp(k_2 t)} \right)$$

Kamau et al.
(1990)

Inactivation models

❖ primary



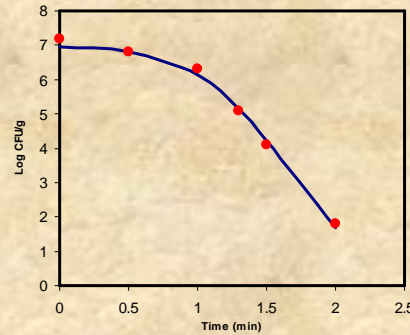
Whiting & Buchanan
(1992)

$$\log \frac{N}{N_0} = \log \left(\frac{F_1(1 + \exp(-k_1L))}{1 + \exp(k_1(t - L))} + \frac{(1 - F_1)(1 + \exp(-k_2L))}{1 + \exp(k_2(t - L))} \right)$$

L – lag or shoulder

Inactivation models

❖ primary



Whiting & Buchanan
(1992)

$$\log \frac{N}{N_0} = \log \left(\frac{F_1(1 + \exp(-k_1L))}{1 + \exp(k_1(t - L))} + \frac{(1 - F_1)(1 + \exp(-k_2L))}{1 + \exp(k_2(t - L))} \right)$$

L – lag or shoulder

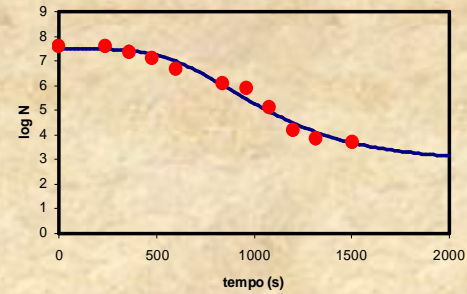
Cole et al.
(1993)

$$\log N = \alpha + \frac{w - \alpha}{1 + \exp\left(\frac{4\sigma(\lambda - \log t)}{w - \sigma}\right)}$$

distribution of heat
sensitivity of
microbial populations

Inactivation models

❖ primary



Baranyi et al.
(1993)

$$\frac{dN}{dt} = -k \alpha(t) \beta(t) N$$

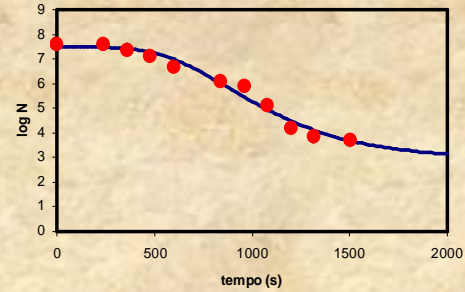
$$N(t = 0) = N_0$$

'tail' function

'lag' function

Inactivation models

❖ primary



Baranyi et al.
(1993)

$$\frac{dN}{dt} = -k \alpha(t) \beta(t) N$$

$$N(t = 0) = N_0$$

'tail' function

'lag' function

Geeraerd et al.
(2000)

$$\frac{dN}{dt} = -k_{\max} k_Q(Q) N$$

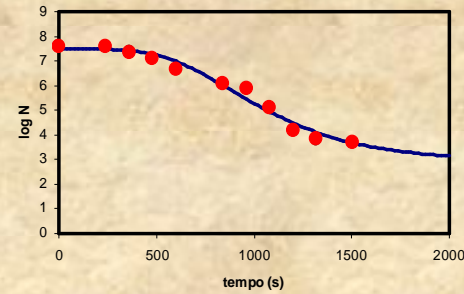
$$\frac{dQ}{dt} = -k_{\max} Q$$

$$\log\left(\frac{N}{N_0}\right) = \log(\exp(-k_{\max} t)) \frac{1 + Q(0)}{1 + Q(0) \exp(-k_{\max} t)}$$

Q – variable related to the physiological state of the cells

Inactivation models

❖ primary



Gompertz

Bhaduri et al (1991)
Linton et al. (1995, 1996)
Xiong et al. (1999)



Listeria monocytogenes

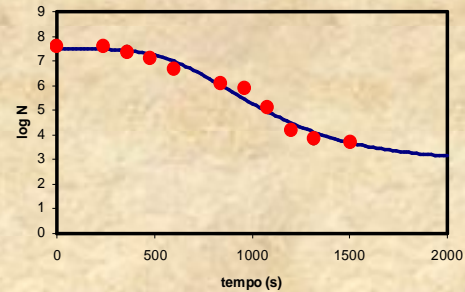
$$\log N = \log N_0 - \log \left(\frac{N_0}{N_{\text{res}}} \right) \exp \left(- \exp \left(\frac{k e}{\log \left(\frac{N_0}{N_{\text{res}}} \right)} (L - t) + 1 \right) \right)$$



reparameterized for inactivation based in Zwietering (1990)

Inactivation models

❖ primary



Gompertz

Bhaduri et al (1991)
Linton et al. (1995, 1996)
Xiong et al. (1999)



Listeria monocytogenes

$$\log N = \log N_0 - \log \left(\frac{N_0}{N_{res}} \right) \exp \left(- \exp \left(\frac{k e}{\log \left(\frac{N_0}{N_{res}} \right)} (L - t) + 1 \right) \right)$$



reparameterized for inactivation based in Zwietering (1990)

Logistic

$$\log N = \frac{c}{1 + \exp(k(t - L))}$$

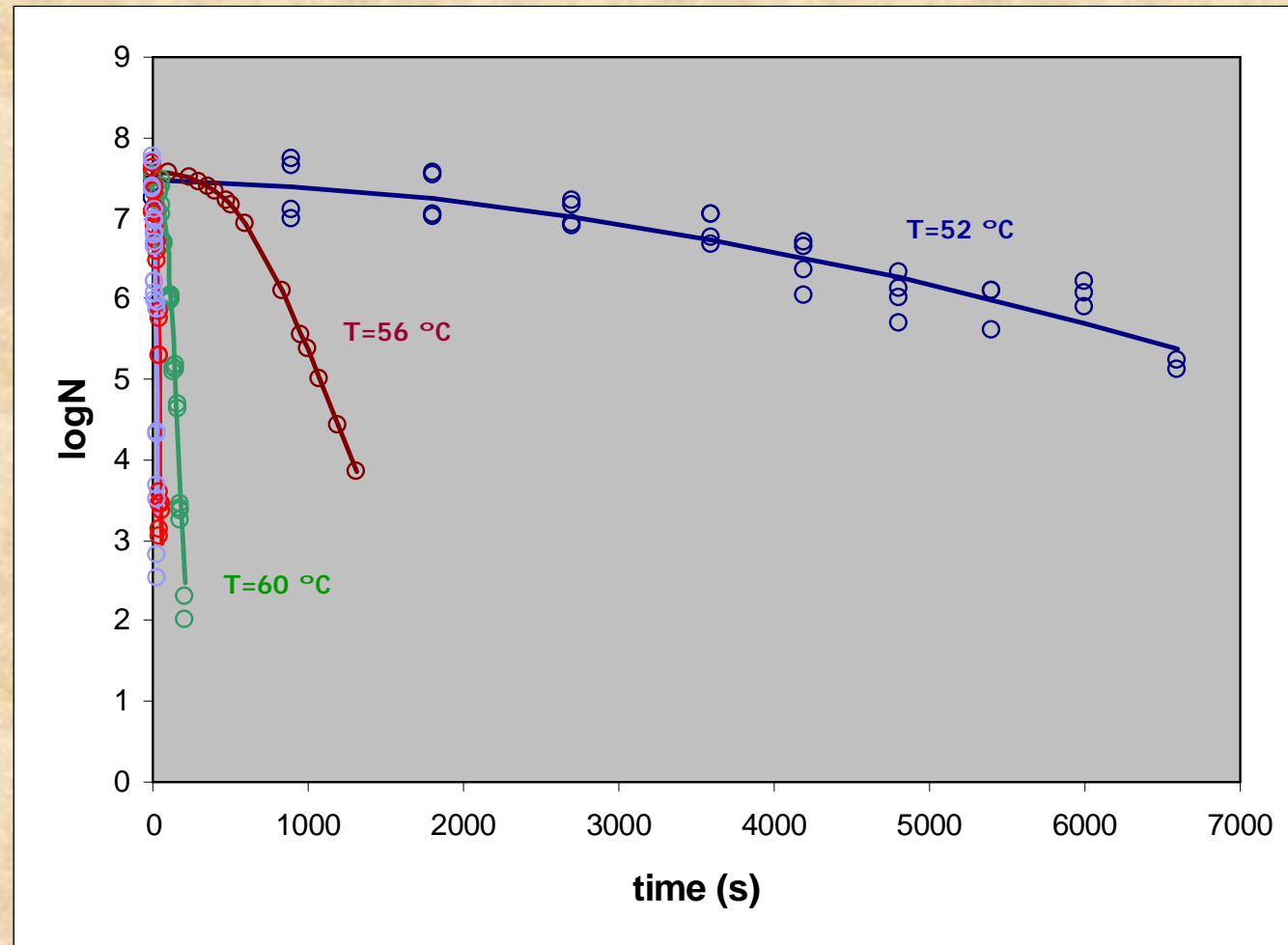
c – constant

Examples

Data of *L. monocytogenes* Scott A at 52,56,60,64,68°C
(24 hours incubation at 5°C in half cream)

Casadei et al. (1998)

Gompertz



Gil (2002)

Statistica 6.0

Examples

Data of *Alicyclobacillus acidoterrestris* spores at 85,91,95,97°C

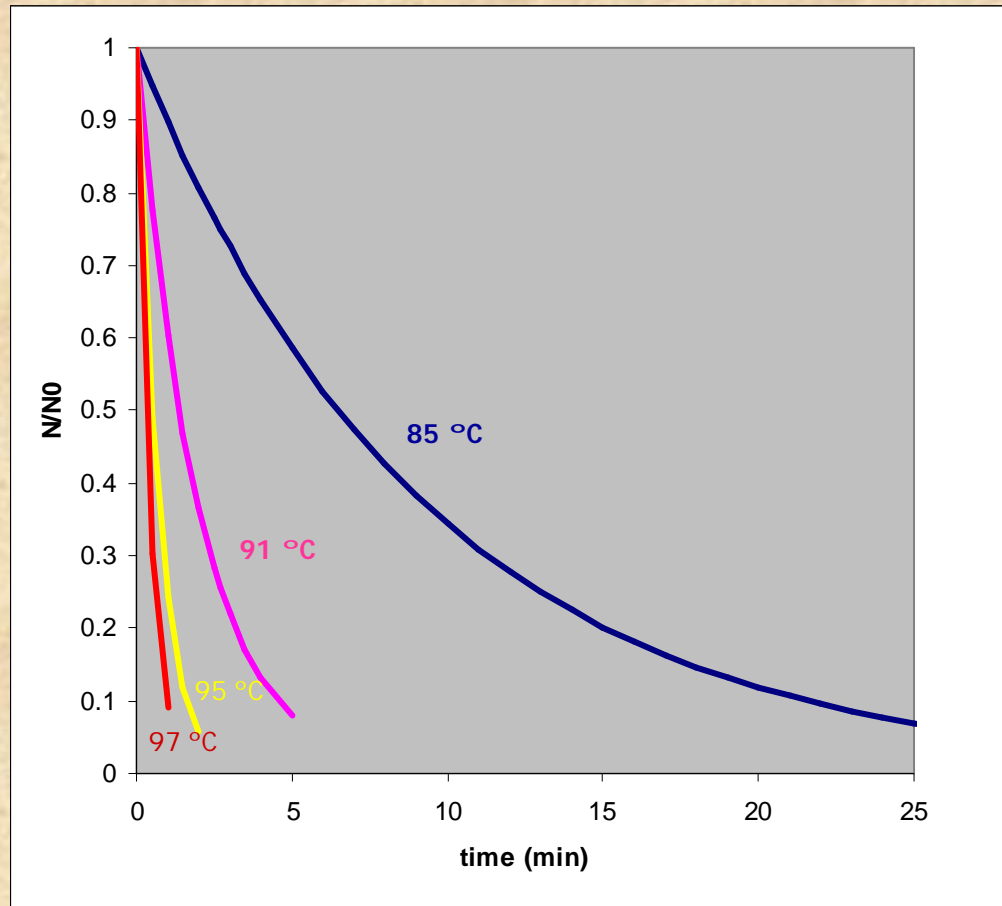
Cupuçu extract pH=3.6 11.3 °Brix

First order



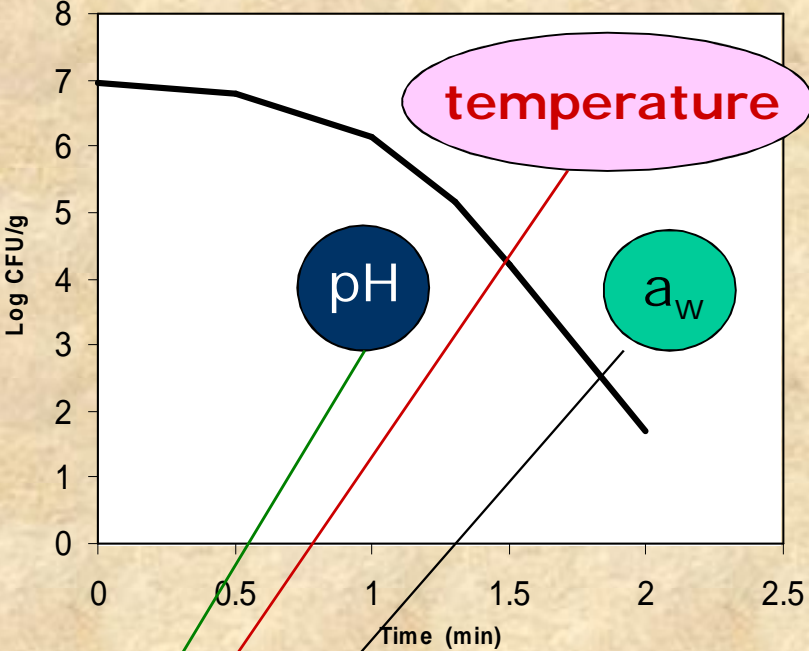
Bigelow

$$\frac{N}{N_0} = 10^{-\frac{t}{D}}$$
$$k = \frac{\ln(10)}{D}$$



Mathematical models

❖ primary



❖ secondary
parameters

Mathematical models

❖ secondary

Arrhenius

$$k = k_0 \exp\left(-\frac{E_a}{RT}\right) \rightarrow \ln k = \ln k_0 - \frac{E_a}{RT}$$

$$k = k_{\text{ref}} \exp\left(-\frac{E_a}{R} \left(\frac{1}{T} - \frac{1}{T_{\text{ref}}}\right)\right)$$

Davey / Arrhenius modified

$$\ln k = C_0 + \frac{C_1}{T} + \frac{C_2}{T^2} + C_3 a_w + C_4 a_w^2$$

“Square-root type models”

Ratkowsky *et al.* (1982)

$$\sqrt{k} = b(T - T_{\text{min}})$$

McMeekin *et al.* (1987)

$$\sqrt{k} = b(T - T_{\text{min}}) \sqrt{(a_w - a_{w_{\text{min}}})}$$

Adams *et al.* (1991)

$$\sqrt{k} = b(T - T_{\text{min}}) \sqrt{(\text{pH} - \text{pH}_{\text{min}})}$$

McMeekin *et al.* (1992)

$$\sqrt{k} = b(T - T_{\text{min}}) \sqrt{(a_w - a_{w_{\text{min}}})} \sqrt{(\text{pH} - \text{pH}_{\text{min}})}$$

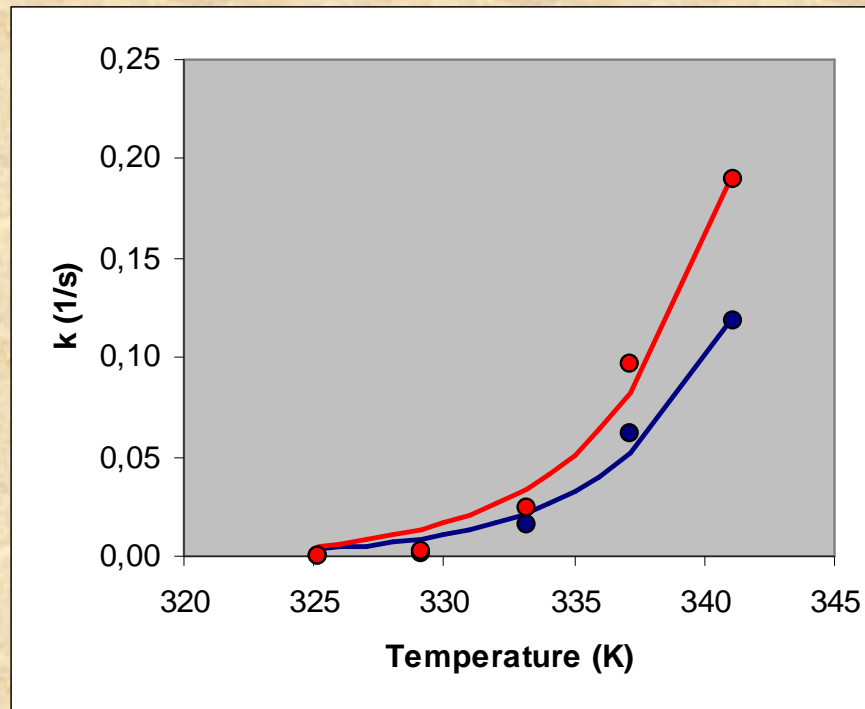
min – minimal value for growth

Examples

Data of *L.monocytogenes* Scott A
(24 hours incubation at 5°C in half cream)

Temperature effect on k

Arrhenius



Gompertz

$$k=0.0216 \exp(-203.3/R^*(1/T-1/333.15))$$

DEa=28.85 kJ/mol

DK_{ref}=4.58x10⁻³ s⁻¹

Logística

$$k=0.0337 \exp(-206.6/R^*(1/T-1/333.15))$$

DEa=27.56 kJ/mol

DK_{ref}=7.31x10⁻³ s⁻¹

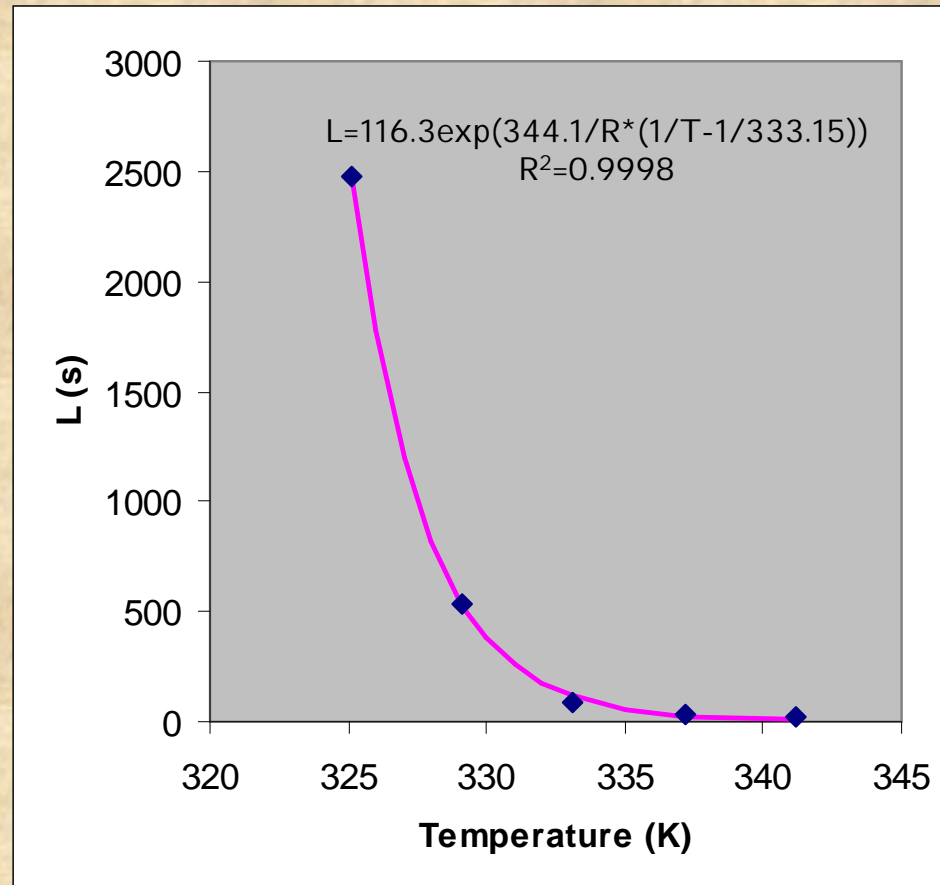
Gil (2002)

Statistica 6.0

Examples

Data of *L.monocytogenes* Scott A
(24 hours incubation at 5°C in half cream)

Temperature effect on lag



$DE_a = 7.485 \text{ kJ/mol}$

$DL_{ref} = 7.595 \text{ s}^{-1}$

Examples

Data of *Alicyclobacillus acidoterrestris* spores at 85,91,95,97°C

Cupuaçu extract pH=3.6 11.3 °Brix

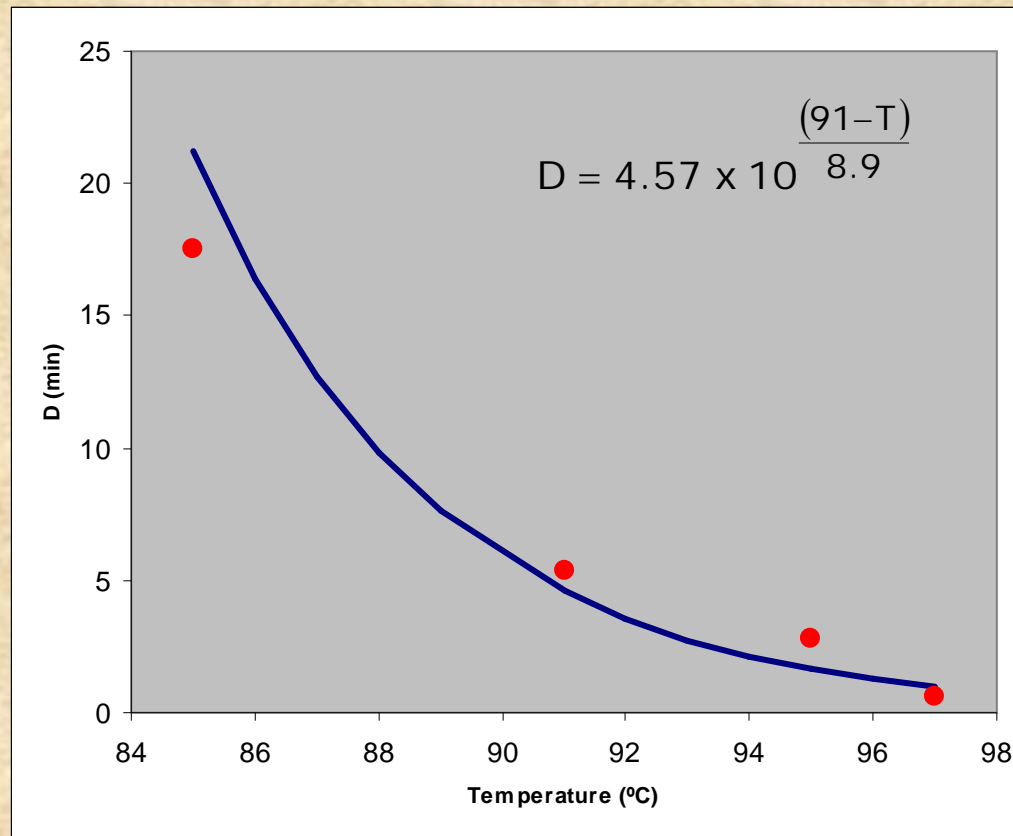
Temperature effect on D-value of *A. acidoterrestris* spores

$$D = D_{ref} 10^{\frac{(T_{ref}-T)}{z}}$$

$T_{ref}=91\text{ }^{\circ}\text{C}$

$DD_{ref}=1.12\text{ min}$

$Dz=1.45\text{ }^{\circ}\text{C}$



Silva (2000)

Examples

Temperature, Soluble Solids and pH effect on D-value of *A. acidoterrestris* spores

malt extract broth

ranges

$$85 < T \text{ (}^\circ\text{C)} < 97$$

$$5 < \text{SS (}^\circ\text{Brix)} < 60$$

$$2.5 < \text{pH} < 6.0$$

Response surface methodology

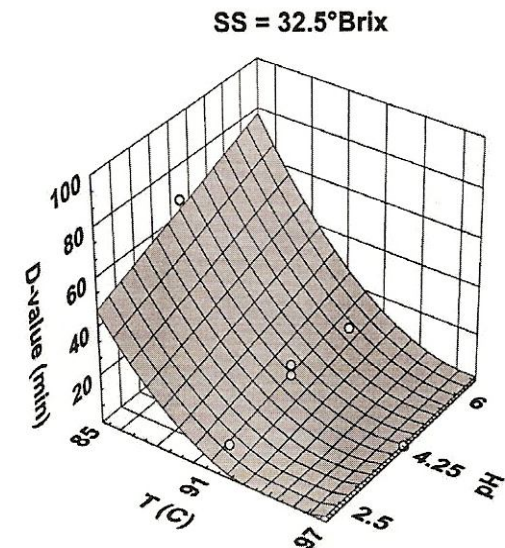
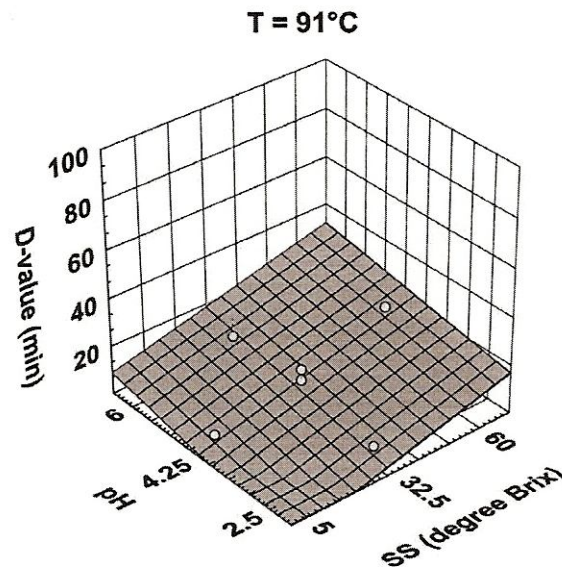
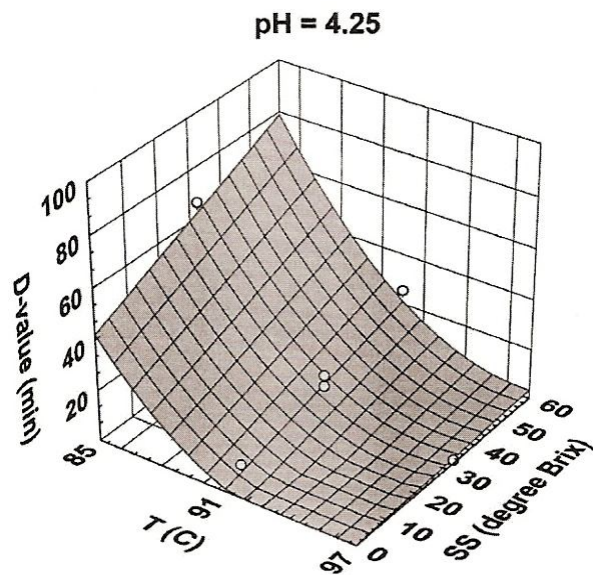


$$D = 4715.1 - (102.96 T) + (0.56042 T^2) + (4.6096 \text{ SS}) - (0.04699 T \text{ SS}) + (57.147 \text{ pH}) - (0.59083 T \text{ pH})$$

Stata 3.0

Examples

Temperature, Soluble Solids and pH effect on D-value of *A. acidoterrestris* spores



Mathematical models

Variable conditions of

temperature

pH

a_w



Complexity !! ... more realistic conditions!!



$$\frac{d(\log N)}{d(\text{time})}$$

Mathematical models

Gompertz

dynamic situation of temperature

$$\downarrow \frac{d(\log N)}{d(\text{time})}$$

$$\log N = \log N_0 - \int_0^t \left[k \exp(1) \exp \left(\frac{k \exp(1)}{\log \left(\frac{N_0}{N_{\text{res}}} \right)} (L - t') + 1 \right) \exp \left(- \exp \left(\frac{k \exp(1)}{\log \left(\frac{N_0}{N_{\text{res}}} \right)} (L - t') + 1 \right) \right) \right] dt'$$

$$k = k_{\text{ref}} \exp \left(- \frac{E_a}{R} \left(\frac{1}{T} - \frac{1}{T_{\text{ref}}} \right) \right)$$

$$L = a \exp \left(b \left(\frac{1}{T} - \frac{1}{T_{\text{ref}}} \right) \right)$$

Mathematical models

Linear

dynamic situation of temperature

$$\downarrow \frac{d(\log N)}{d(\text{time})}$$

$$\frac{N}{N_0} = 10^{\left(\frac{-1}{D_{T_{\text{ref}}}} \int_0^{PT} 10^{\frac{T-T_{\text{ref}}}{z}} dt \right)}$$

$$D = D_{\text{ref}} 10^{-\frac{1}{z}(T-T_{\text{ref}})}$$

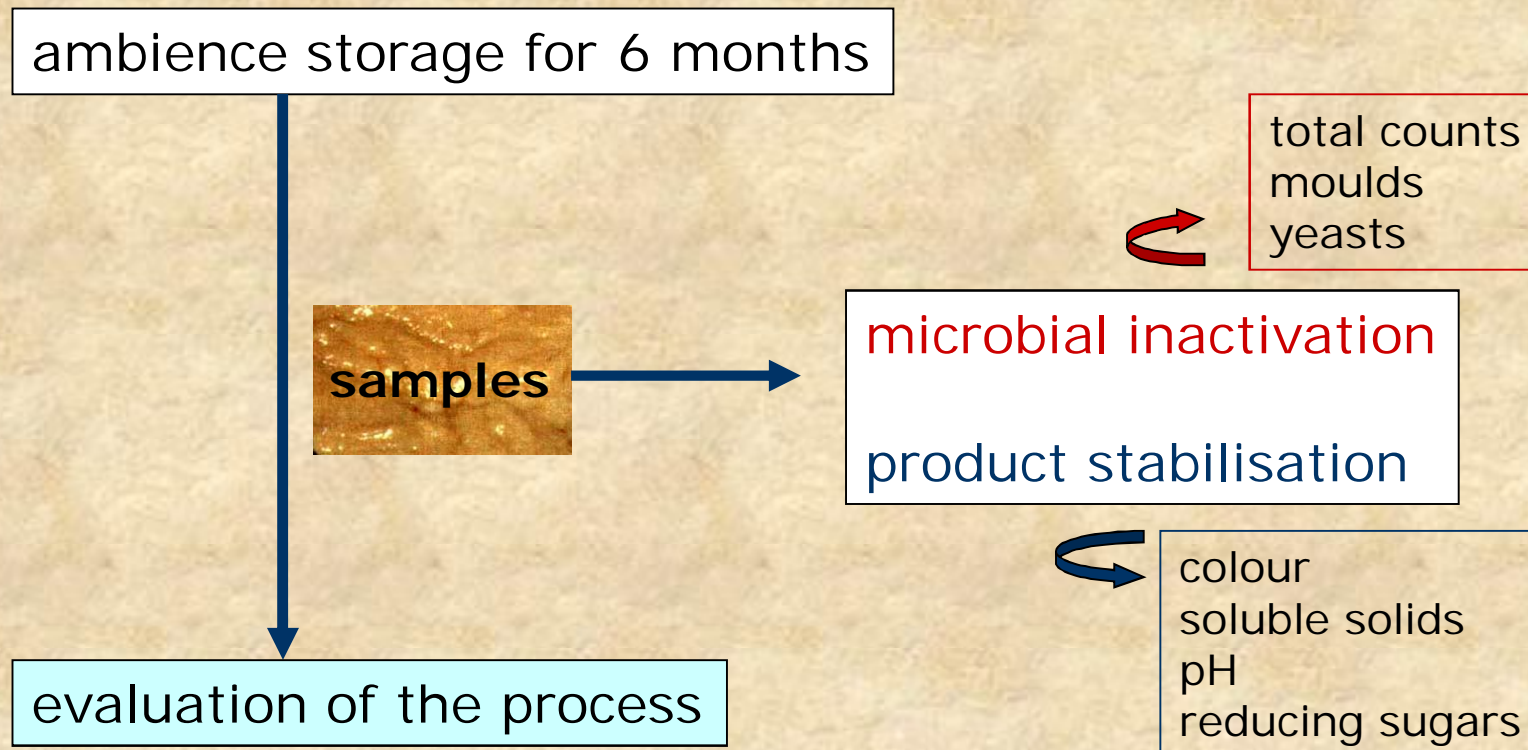
different temperature histories

approach by Vieira et al. (2002)

Cupuaçu nectar

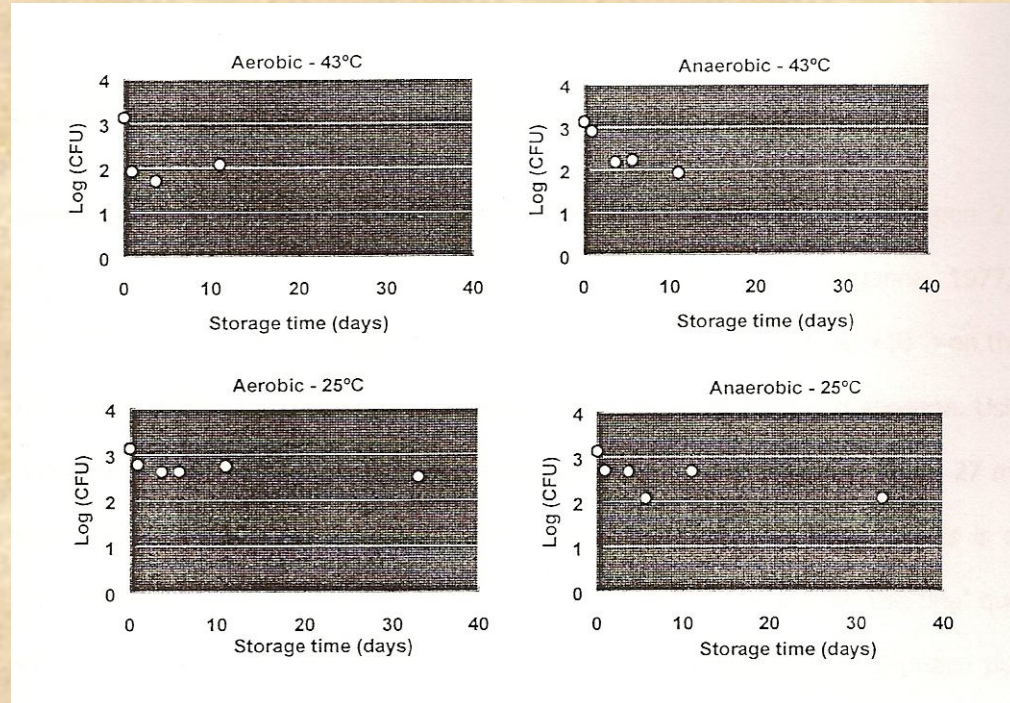
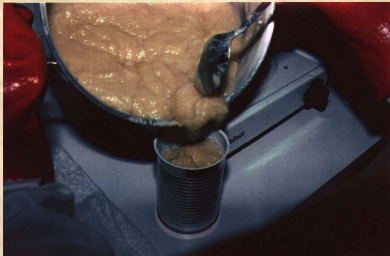
Design and optimization of pasteurization processes

reminding



Design and optimization of pasteurization processes

Criterion



$$\frac{N}{N_0} = 0.1$$

Alicyclobacillus acidoterrestris spores

Mathematical models

❖ tertiary

softwares

Microbial growth

Shelf life prediction

Microbial inactivation

lacunas

"BUGDEATH" (QLRT-2001-01415)



Micrograph of a Salmonella bacterium

Predicting the reduction in microbes on the surface of foods during pasteurisation.

- [Tell me more about the Bugdeath project.](#)
- [What are the objectives of the Bugdeath project?](#)
- [Who are the project partners?](#)
- [Meetings](#)
- [Industrial Advisory Group \(IAG\)](#)
- [Partner area of web site \(specifically for project partners - password needed to enter\)](#)

Bugdeath

BUGDEATH is a research project funded by the European Commission to produce accurate predictive models of the reductions in microbial numbers that can be achieved on the surface of foods during surface pasteurisation processes.

Food poisoning is increasing throughout the European Union (EU). Over 60% of outbreaks are associated with meat, fresh fruit and salad vegetables. Most of the contamination by pathogenic and spoilage organisms is present on the surface of foods at the time of harvesting or is transferred to the surfaces during slaughter and processing. Accurate microbial death models would be of considerable help to the food industry in the development of surface pasteurisation systems for meat, fruit and vegetables. This will in turn lead to safer foods with improved quality and shelf life.

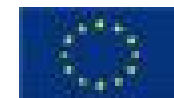


Personnel involved in Bugdeath from left to right

Software Program



'Bugdeath' - funded by the European Commission under the EC Framework 5;
Quality of Life and Management of Living Resources Programme



First screen – product/microorganism

BugDeath [Minimize] [Maximize] [Close]

Product | Process | Output

Temperature variation | Microbial load variation | Data Table

Product: Beef

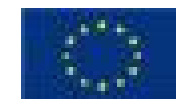
Diffusivity	1.23e-07	Conductivity	4.5e-01
Product thickness (m)	0.016		
Init. Product Temp. (°C)	13.4		
Sample Diameter (m)	0.05		
Water activity	0.45		

Microorganism: *S. typhimurium*

D (min)	6.6e+1	Safe Count	1.e+0	Initial Count	10000000
	7		0.2		57.2
Z (°C)		Z(aw)	0.2206	R. Temp. (°C)	2.279372077
		C1		Q0	

Surface Temperature Medium Temperature

'Bugdeath' - funded by the European Commission under the EC Framework 5;
Quality of Life and Management of Living Resources Programme



Second screen – process

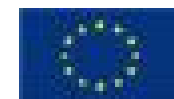
The screenshot shows the 'BugDeath' software interface with the 'Process' tab selected. The main window contains several sections:

- Calculation type:** Radio buttons for 'Surface Temp' (selected) and 'Microbial Death'.
- Thermal Process:** Radio buttons for 'Dry' (selected) and 'Wet'.
- Air Properties:** Input fields for Density (101323), Pressure (Pa) (0.00002), Viscosity (0.028), and Conductiv.
- Equipment Parameters:** Input fields for Air Veloc. (20), Turbulence (0.25), and Transf. C (5).
- Heating Regimen or Surf. Temperature:** Radio buttons for 'Simple' (selected) and 'Complex', each with a 'Define...' button.
- Tabulated data:** A 'Load...' button.
- Temp. Bott (°C):** An input field with the value 40.

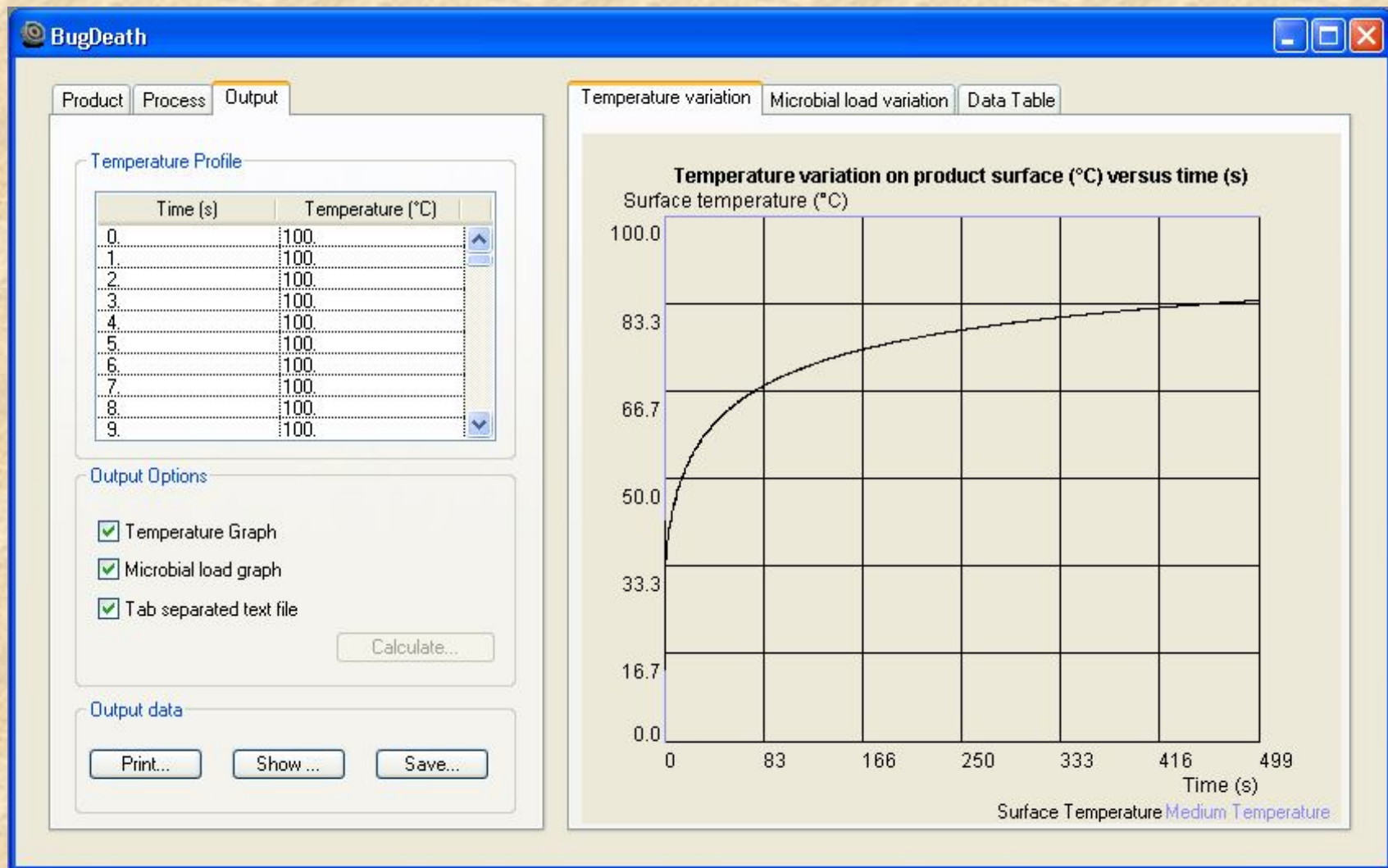
A 'Simple Heating Regimen' dialog box is open in the foreground, showing the following parameters:

- Parameters:**
 - Total Process Time (s): 500
 - Holding temperature (°C): 100
- Buttons: 'Cancel' and 'OK'.

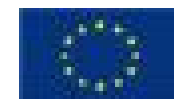
At the bottom right of the main window, there are labels for 'Surface Temperature' and 'Medium Temperature'.



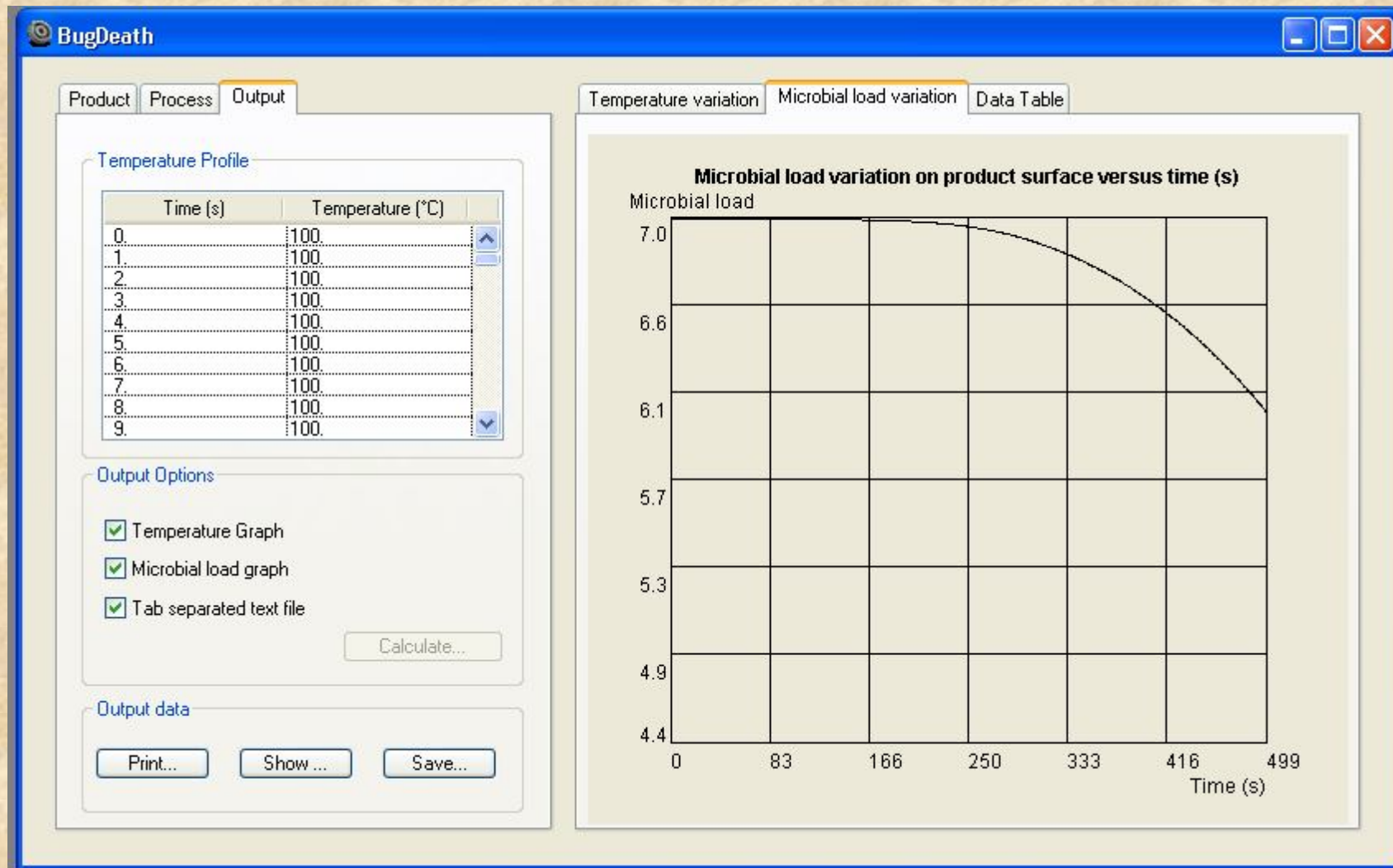
Output – graphic/temperature



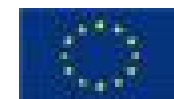
'Bugdeath' - funded by the European Commission under the EC Framework 5;
Quality of Life and Management of Living Resources Programme



Output – graphic/microbial load



'Bugdeath' - funded by the European Commission under the EC Framework 5;
Quality of Life and Management of Living Resources Programme



Output – data table

The screenshot shows the 'BugDeath' software interface. The 'Data Table' tab is active, displaying the following data:

Time (s)	Medium Temp. (°C)	Surface Temp. (°C)	Microbial Load
0	0	14.02522	7
0.6081229	100	39.29868	6.991117
1	100	31.74754	6.991117
1.608123	100	35.68345	6.991117
2	100	36.00534	6.991117
2.608123	100	36.9512	6.991117
3	100	38.14414	6.991117
3.608123	100	38.62585	6.991117
4	100	39.78456	6.991117
4.608123	100	40.16022	6.991117
5	100	41.19636	6.991117
5.608123	100	41.524	6.991117
6	100	42.4504	6.991117
6.608123	100	42.74452	6.991117
7	100	43.58093	6.991117
7.608123	100	43.84836	6.991117
8	100	44.61078	6.991117
8.608123	100	44.85613	6.991117
9	100	45.55682	6.991117
9.608123	100	45.78353	6.991117
10	100	46.43196	6.991117
10.60812	100	46.64271	6.991116
11	100	47.2463	6.991116
11.60812	100	47.44323	6.991116
12	100	48.0079	6.991116
12.60812	100	48.19275	6.991116
13	100	48.72329	6.991115
13.60812	100	48.89746	6.991115
14	100	49.39783	6.991115

'Bugdeath' - funded by the European Commission under the EC Framework 5;
Quality of Life and Management of Living Resources Programme



Predictive microbiology

Drawbacks

- microbial interaction
- natural strains diversity
- complexity of food structure
- food/microorganism
- modelling of the 'lag' phase
- modelling of the 'tail' phase
- predictions in real and varying environmental conditions

Future challenges

non-thermal treatments

safety



efficient microbial inactivation

quality



maximum quality retention

avoiding the negative effects of heat
at tissues level

Future challenges

non-thermal treatments

- ozone



aqueous solution

atmosphere



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New Processing Technologies for Frozen Fruits and Vegetables

Future challenges

non-thermal treatments

- ultrasounds + heat treatments
thermosonication



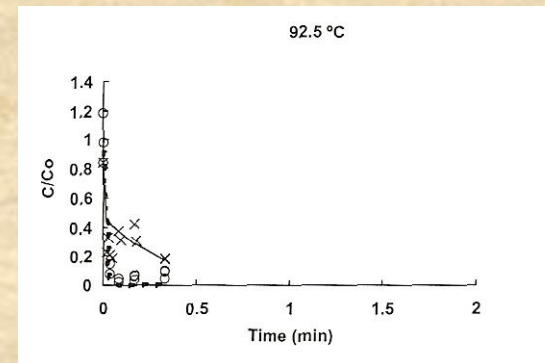
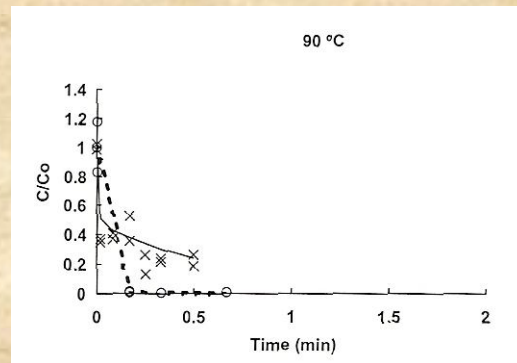
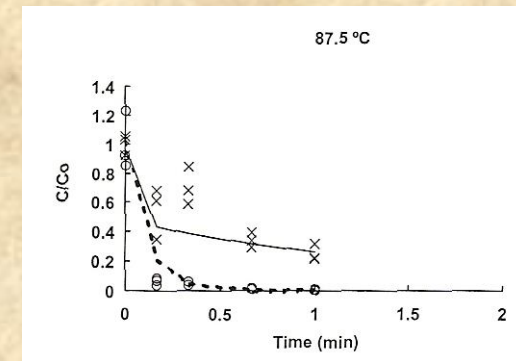
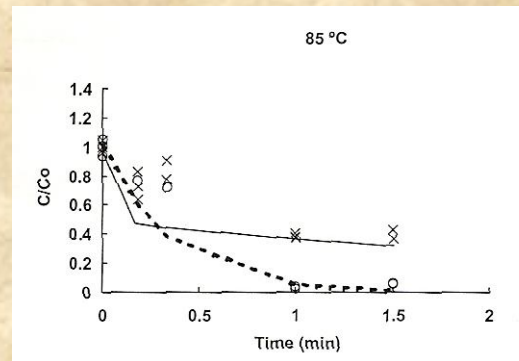
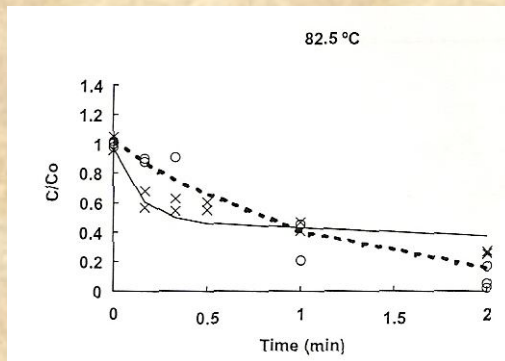
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New Processing Technologies for Frozen Fruits and Vegetables

Future challenges

thermosonication

peroxidase inactivation in watercress



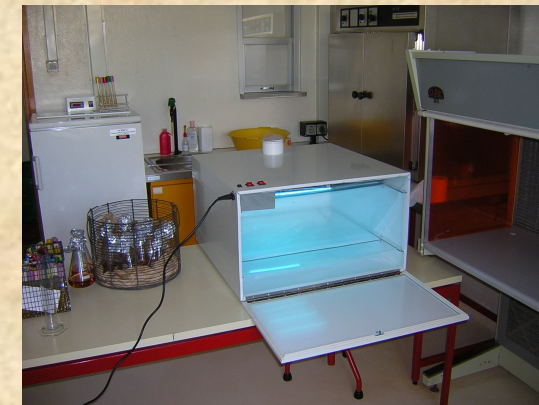
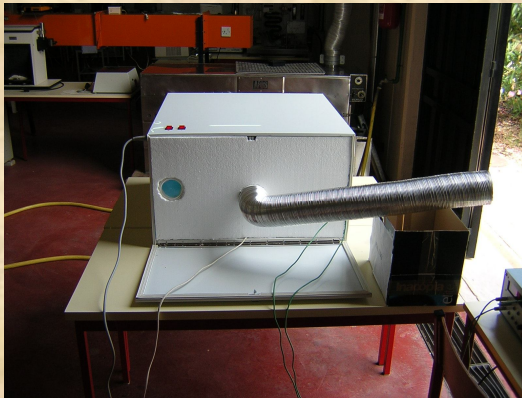
x blanching
o thermosonication

Future challenges

non-thermal treatments



UV radiation



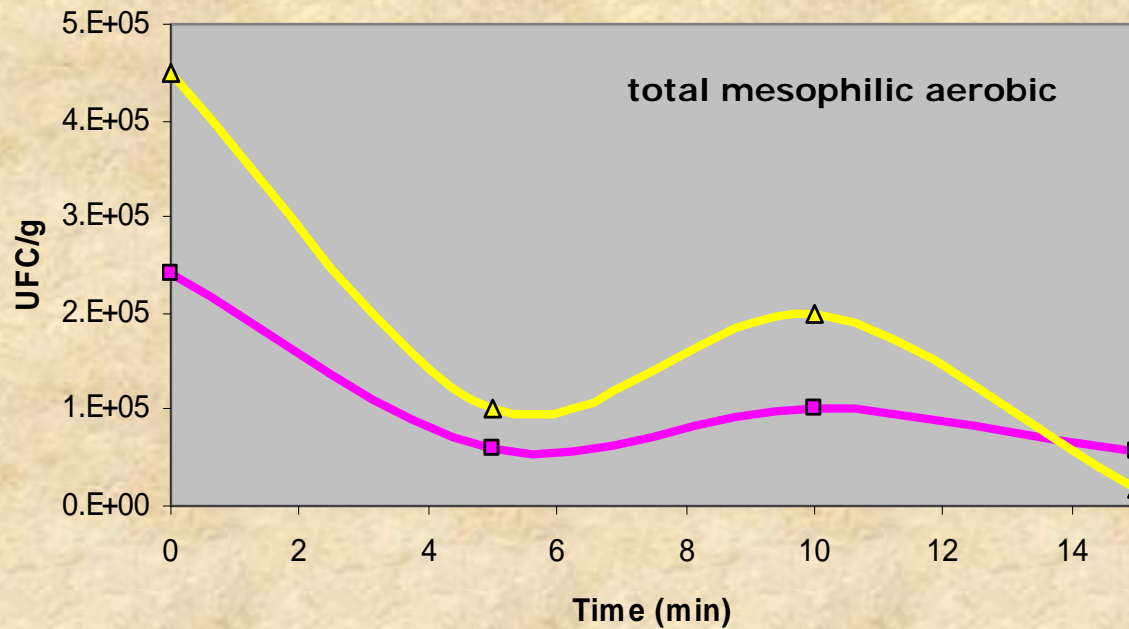
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New Processing Technologies for Frozen Fruits and Vegetables

Future challenges

non-thermal treatments

● UV radiation



8.4 W UV-C
courgettes



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New Processing Technologies for Frozen Fruits and Vegetables

Spore forming bacteria
emerging and re-emerging issues

Summer Meeting 2005

Thank you

Teresa Brandão

Cristina Silva



UNIVERSIDADE CATÓLICA PORTUGUESA
Escola Superior de Biotecnologia

Brighton 4th – 7th July 2005