

Escola Superior de Biotecnologia
Universidade Católica Portuguesa



Microstructural changes during fruit drying - correlation between fundamental studies, with air drying and solar drying applications.

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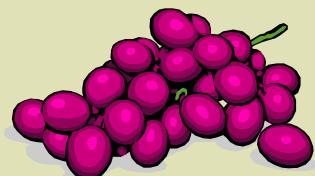
Introduction



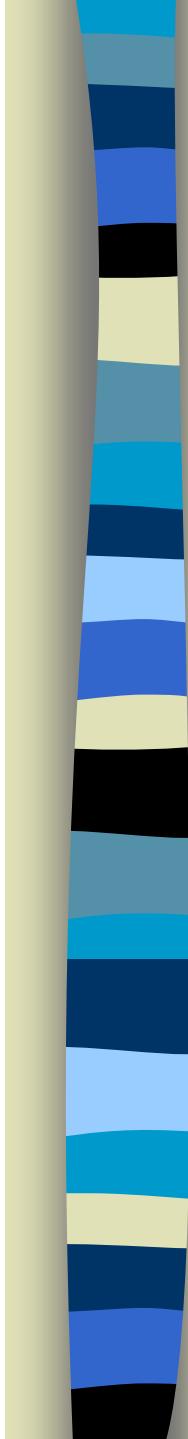
Solar Drying



Solar dryer.

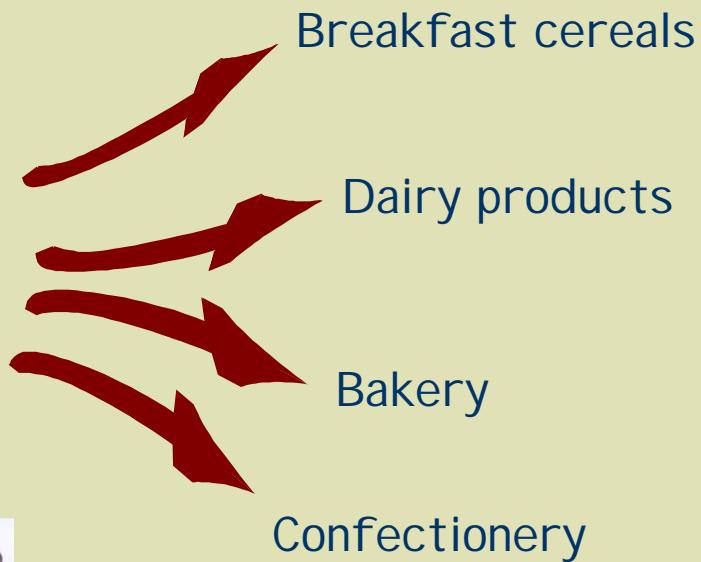


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Introduction

Diversified products





Introduction

Integrated model

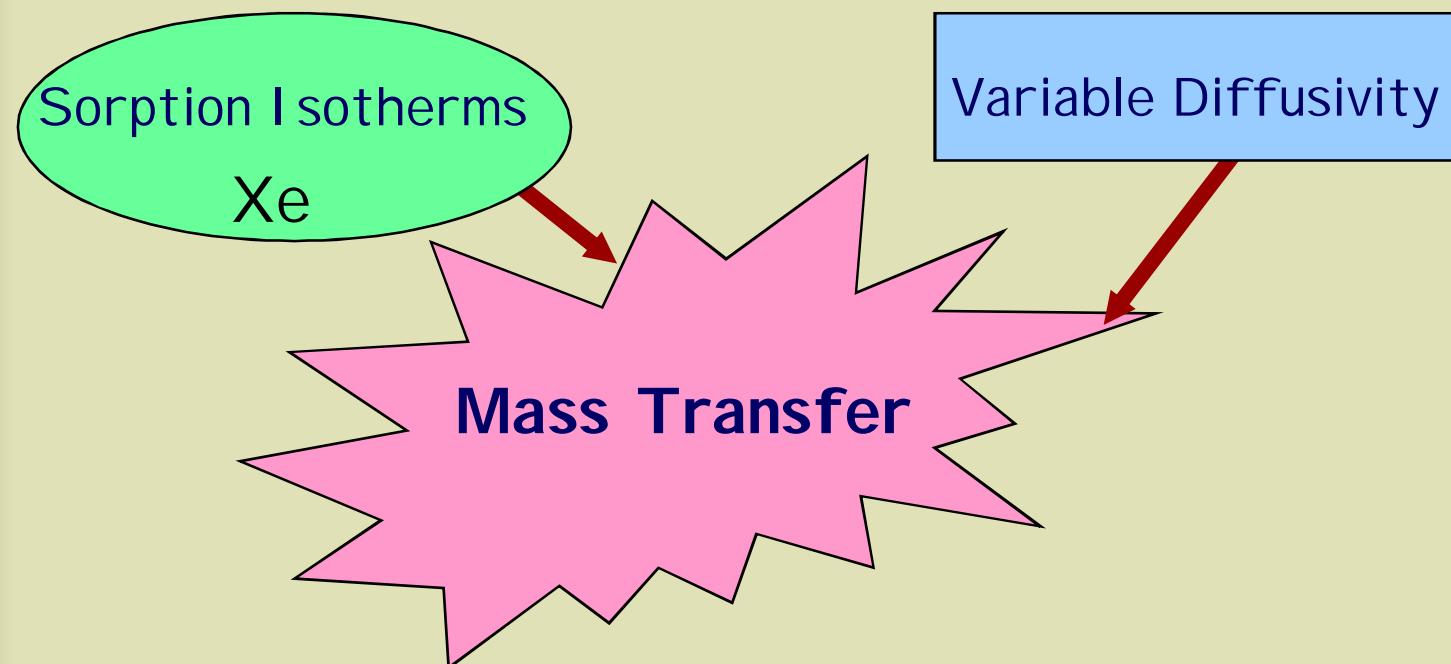


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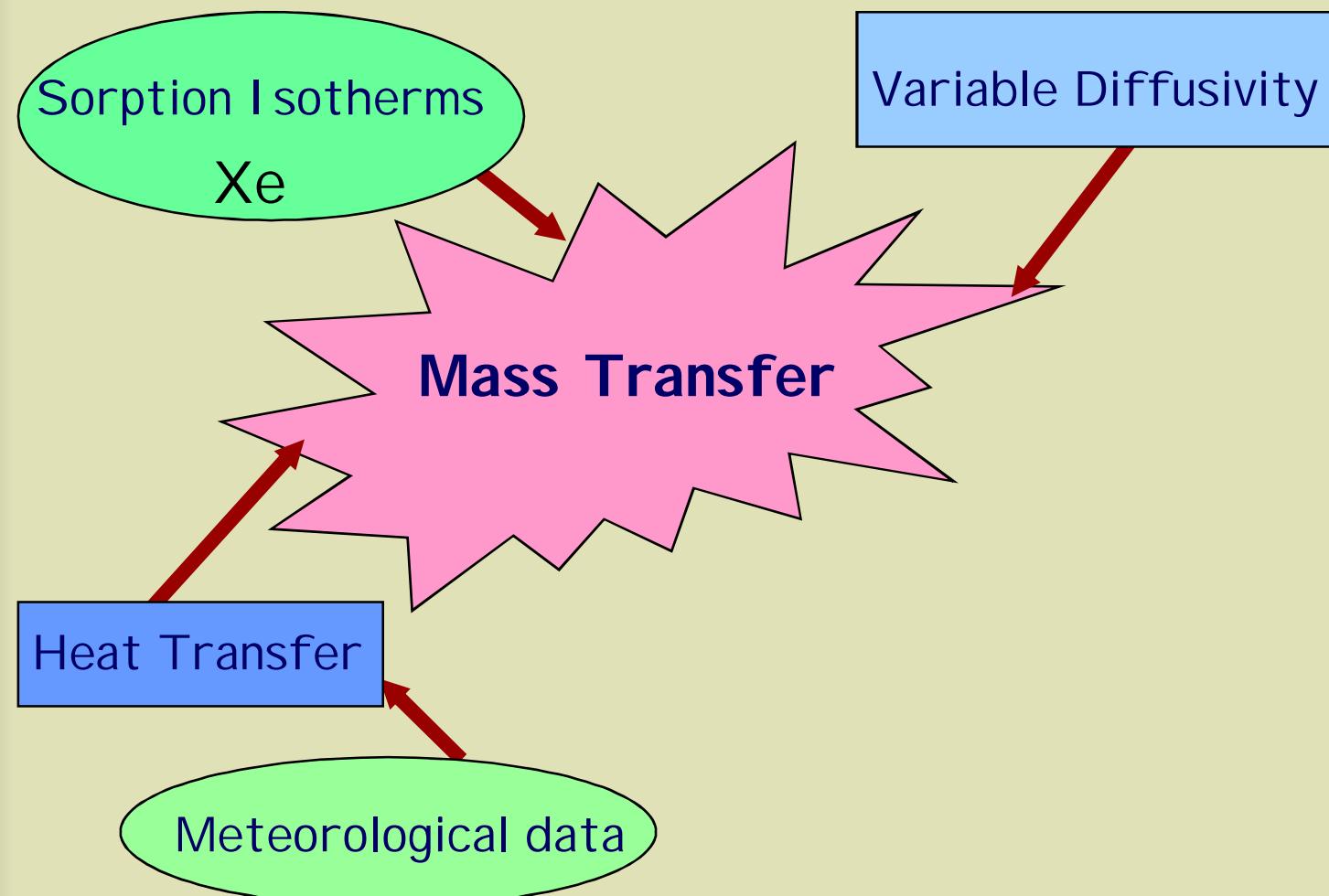
Introduction

Integrated model



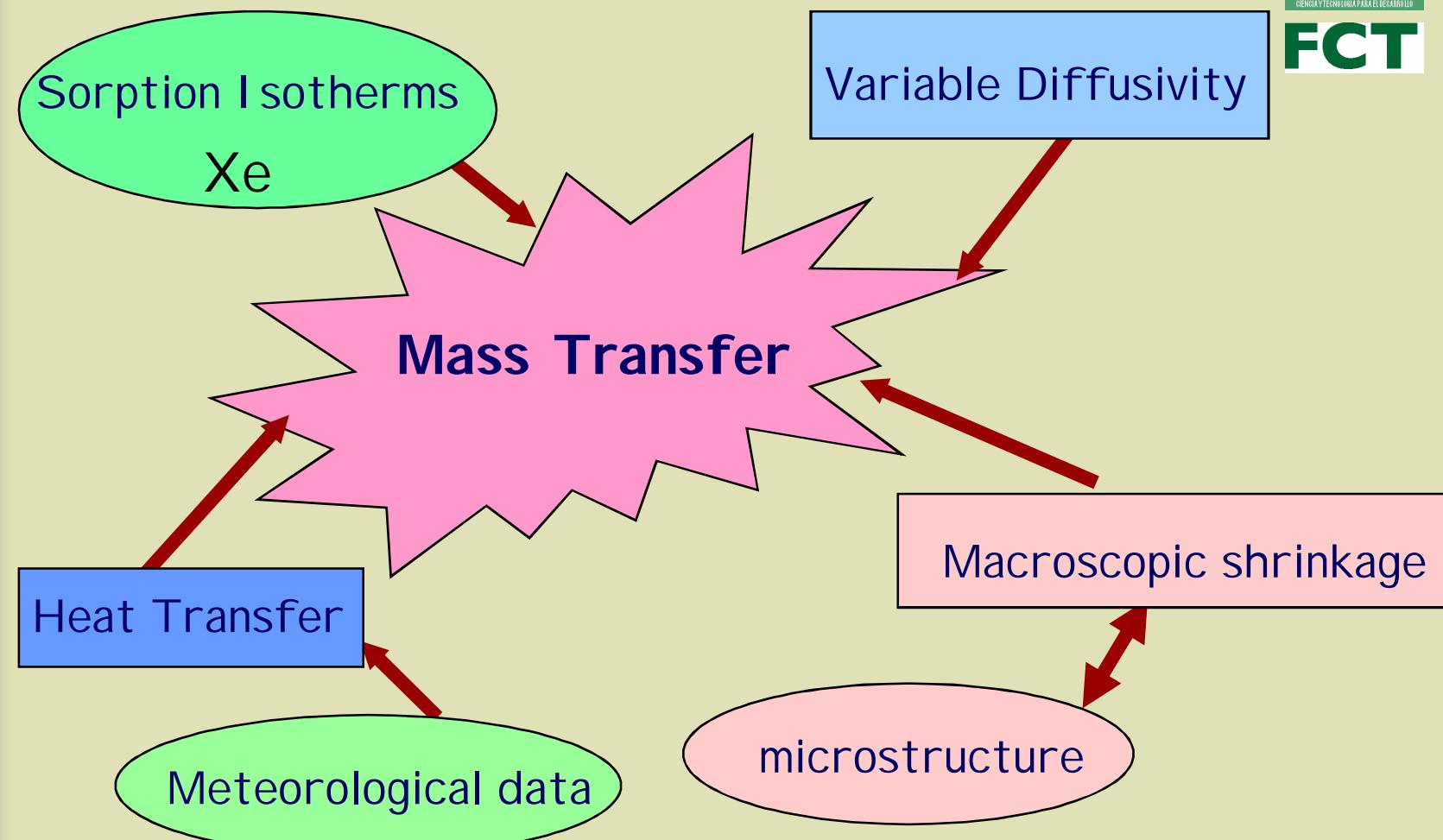
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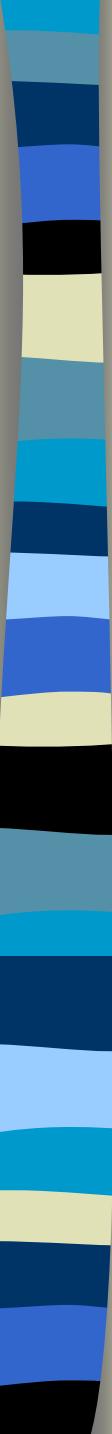
Integrated model



Introduction

Integrated model

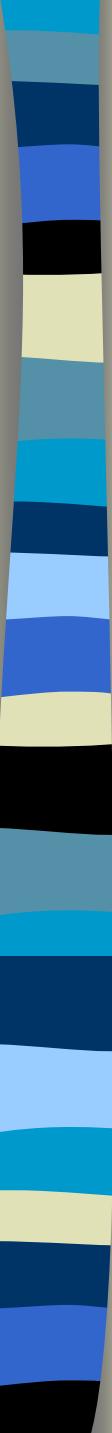




Introduction

Predict and simulate the drying behaviour:





Introduction

Predict and simulate the drying behaviour:

- ◆ Mechanistic models are more complex, but allow accurate predictions (Mulet, 1994).
- ◆ Empirical models are much simple, but appropriate to practical uses (e.g. dryers design).

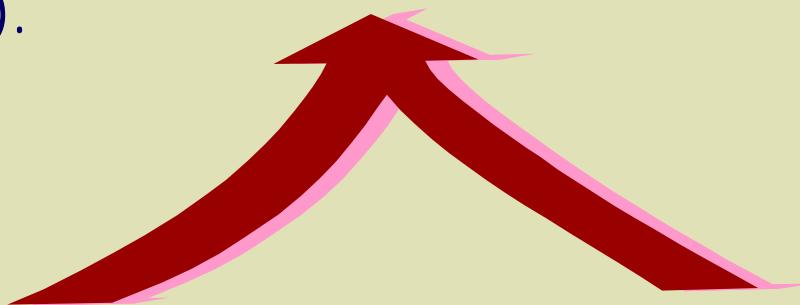


Introduction



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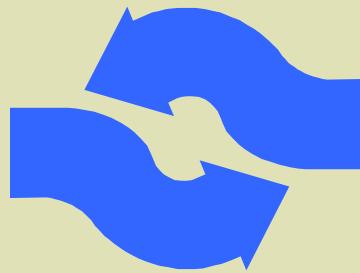


Balance of the advantages and disadvantages, depending on the final purpose.

Introduction



Physical properties

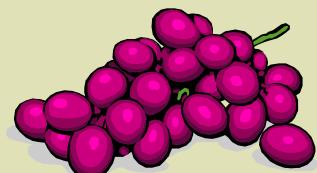


Drying mechanisms

Microstructure

Quality changes

e.g. Texture



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Mass Transfer

Short constant-rate period

Long falling-rate period

Fick's 2nd law



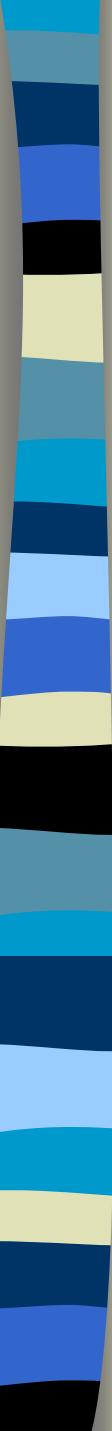
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Mass Transfer

Fick's 2nd law

- ◆ Water concentration at the surface constant
- ◆ Sphere:

$$\frac{X - X_e}{X_o - X_e} = \frac{6}{\pi^2} \sum_1^{\infty} \frac{1}{n^2} \exp(-n^2 \pi^2 \frac{D_{eff} t}{r^2})$$



Mass Transfer



- ◆ Consider uniform temperature inside the food

{ non-isotropic characteristics of the medium
porosity

$$\rightarrow D_{\text{eff}}$$

(effective diffusivity)



variable

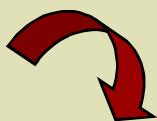


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Effective diffusivity

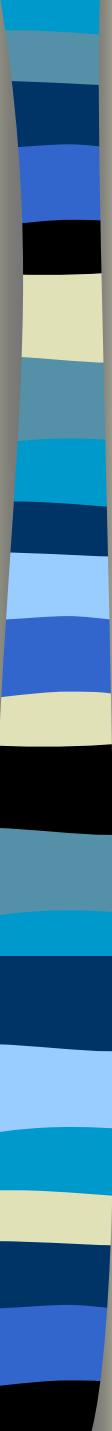
D_{eff} varies:

- considerably with **water content**
(Karathanos, Villalobos and Saravacos, 1990)
- with **temperature**



Arrhenius law:

$$D = D_{\text{ref}} \exp \left[-\frac{E_a}{R} \left(\frac{1}{T} - \frac{1}{T_{\text{ref}}} \right) \right]$$



Effective diffusivity



- ◆ Dependence on water content is usually neglected
- ◆ Proposed models:
exponential, power-law, gamma function

Exponential are the most used models





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Effective diffusivity

$$D_{\text{eff}} = \exp(a + bX + cX^2)$$

(Vásquez, Chenlo, Moreira & Costoyas, 2000)

$$D_{\text{eff}} = \exp(d + e/T + fX)$$

(Mulet et al., 1989)

$$D_{\text{eff}} = D_o \exp(-D_T/T) \exp(-D_x/X)$$

(Maroulis, Kiranoudis & Marinos-Kouris, 1995)

Effective diffusivity



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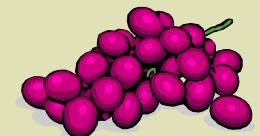
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Experiments performed in a convective dryer.



Pilot plant convective tray drier (Armfield UOP8).



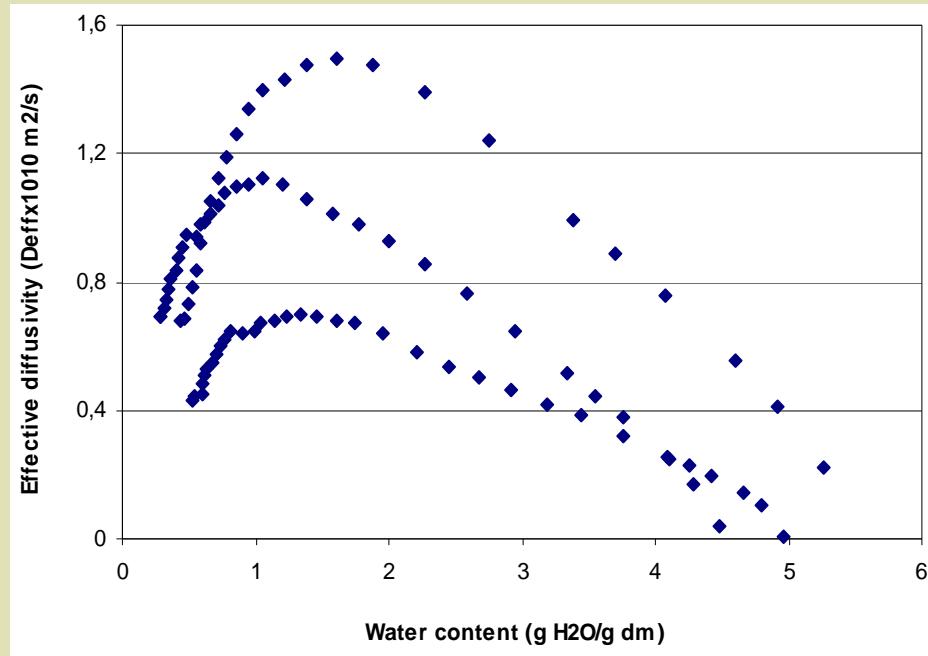
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Effective diffusivity

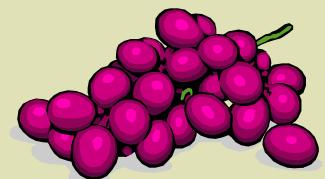


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Data similar to Raghavan et al., 1995



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Equilibrium value

Sorption isotherms

The G.A.B. model is recently widely applied:

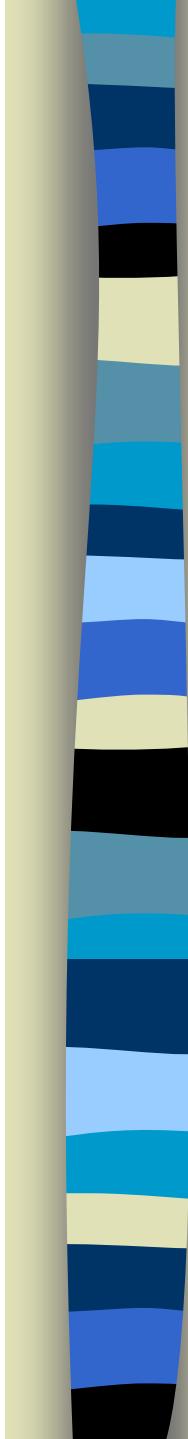
$$\frac{X_e}{X_m} = \frac{C k a_w}{(1 - k a_w)(1 - k a_w + C k a_w)}$$

$$C = C_0 \exp\left(\frac{\Delta H_c}{RT}\right)$$

$$k = k_0 \exp\left(\frac{\Delta H_k}{RT}\right)$$



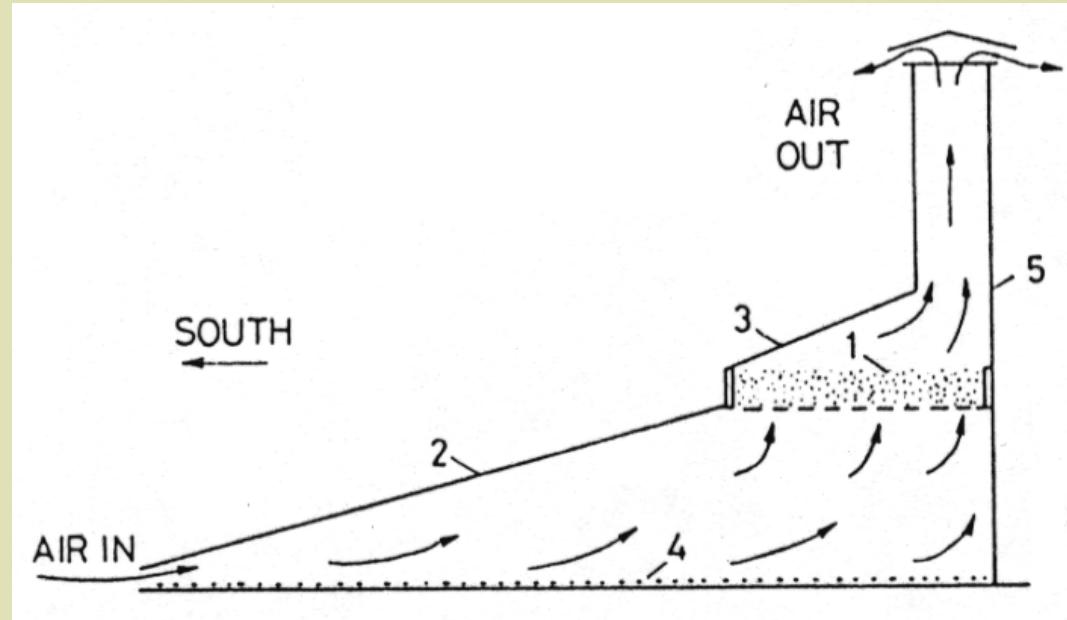
Temperature dependent

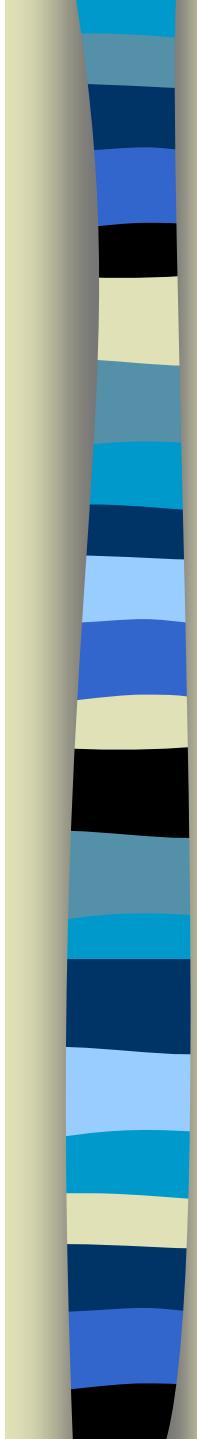


Heat Transfer



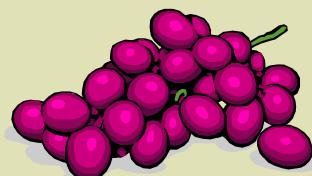
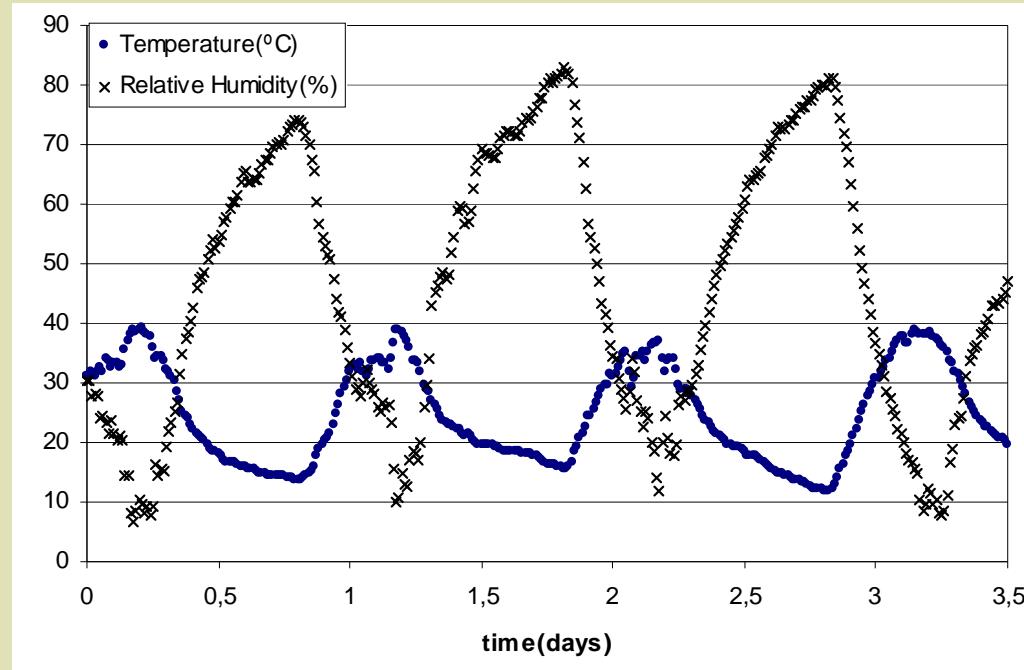
Solar **radiation** originates a 'greenhouse' effect





Heat Transfer

Air conditions inside a solar drier :



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Heat Transfer

Global energy balance :

$$\frac{d(mC_p T)}{dt} = \alpha Q_s - hA(T - T_a) - \frac{d(\lambda m)}{dt} - A \varepsilon \sigma (T^4 - T_a^4)$$

Heat Transfer



Global energy balance :

$$\frac{d(mC_p T)}{dt} = \alpha Q_s - hA(T - T_a) - \frac{d(\lambda m)}{dt} - A \varepsilon \sigma (T^4 - T_a^4)$$



energy gained

Heat Transfer



Global energy balance :

$$\frac{d(mC_p T)}{dt} = \alpha Q_s - hA(T - T_a) - \frac{d(\lambda m)}{dt} - A \varepsilon \sigma (T^4 - T_a^4)$$

energy gained

absorved
radiant energy

Heat Transfer



Global energy balance :

$$\frac{d(mC_p T)}{dt} = \alpha Q_s - hA(T - T_a) - \frac{d(\lambda m)}{dt} - A \varepsilon \sigma (T^4 - T_a^4)$$

energy gained /
absorbed convective
radiant energy heat loss

Heat Transfer



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Global energy balance :

$$\frac{d(mC_p T)}{dt} = \alpha Q_s - hA(T - T_a) - \frac{d(\lambda m)}{dt} - A \varepsilon \sigma (T^4 - T_a^4)$$

energy gained

absorbed
radiant energy

convective
heat loss

evaporation
heat loss

Heat Transfer



Global energy balance :

$$\frac{d(mC_p T)}{dt} = \alpha Q_s - hA(T - T_a) - \frac{d(\lambda m)}{dt} - A \varepsilon \sigma (T^4 - T_a^4)$$

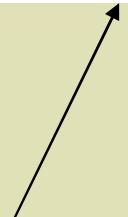


Heat Transfer

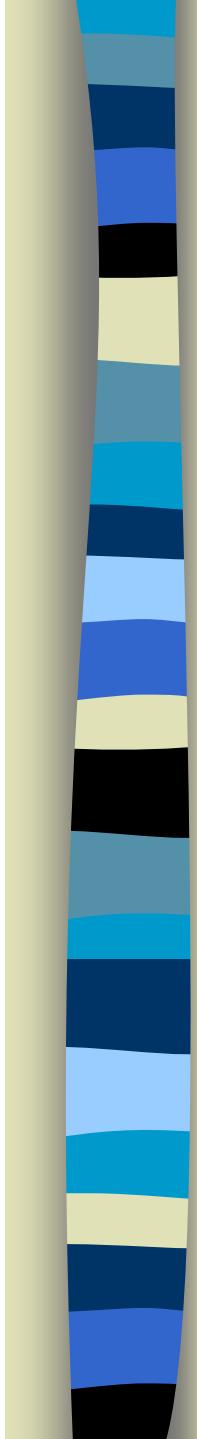


Global energy balance :

$$\frac{d(mC_p T)}{dt} = \alpha Q_s - hA(T - T_a) - \frac{d(\lambda m)}{dt} - A \varepsilon \sigma (T^4 - T_a^4)$$



obtained from **meteorological data**



Heat Transfer

- Lack of data on radiation properties of foods



Heat Transfer

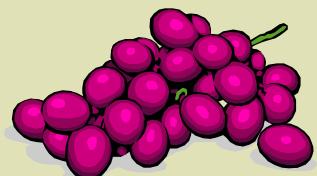
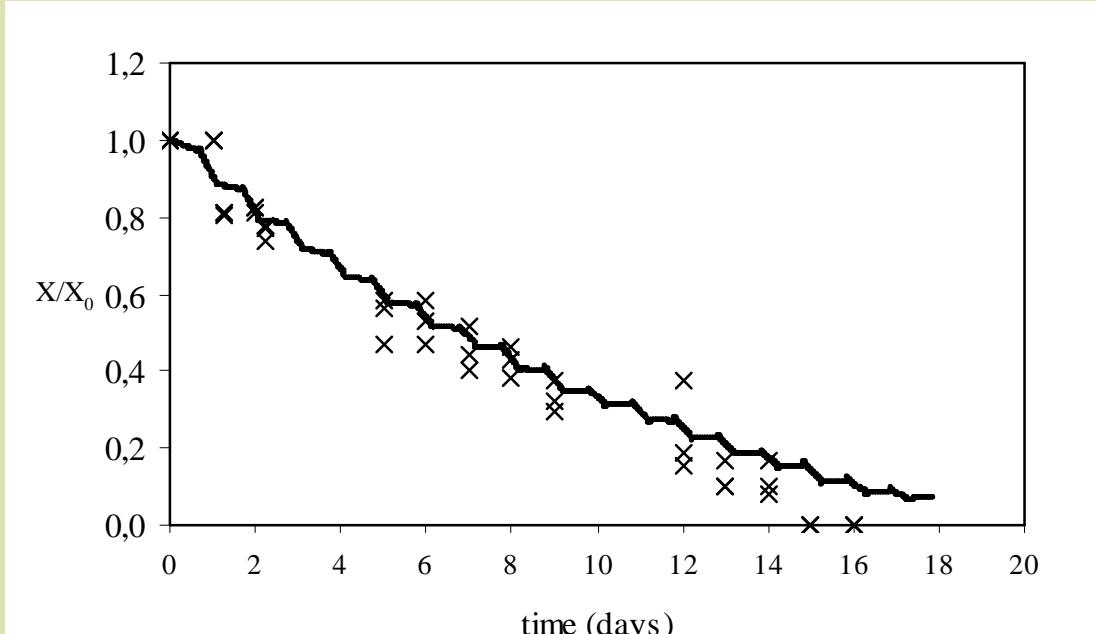


- Lack of data on radiation properties of foods
- Cp is strongly dependent on water content
 - compilation on Sweat (1986)
 - most of the research on freezing and refrigeration !!!



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Simulation under dynamic conditions on a pilot scale and Data of solar dryer



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Shrinkage

Loss of water

shrinkage



reduction in cellular dimensions

Macroscopic Shrinkage

Commonly defined:

$$\frac{V}{V_0}$$



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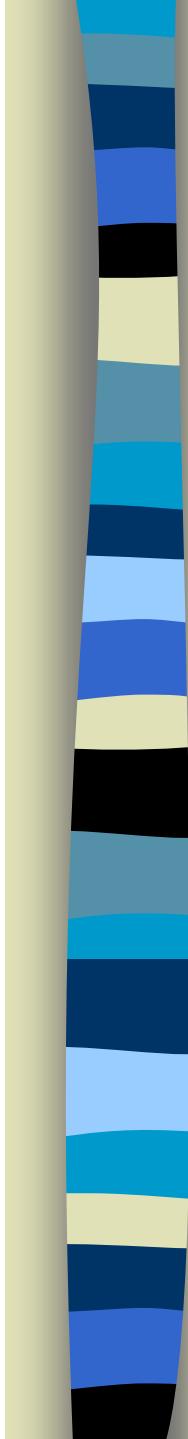
Macroscopic Shrinkage

Measurement :

- direct with a calliper
- picnometry with organic solutions
- photography and image analysis:



Grape shrinkage under dynamic conditions.

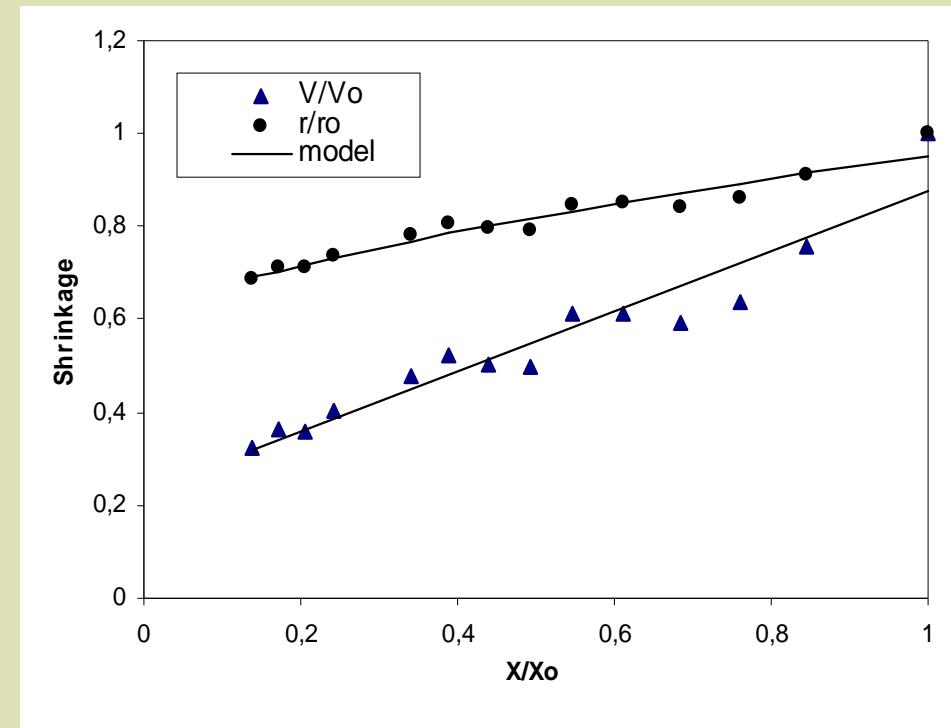


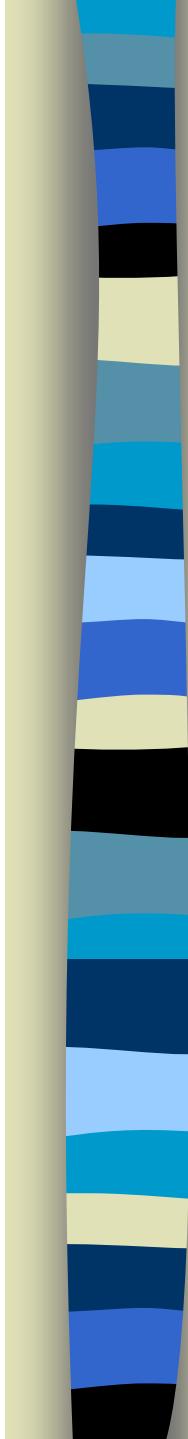
Macroscopic Shrinkage



Dependence of shrinkage on water content
common linear relationship

$$\frac{V}{V_0} = a + bX$$





Microscopic Shrinkage



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Decrease in water content



Loss of turgor pressure



Mainly from vacuolar compartment

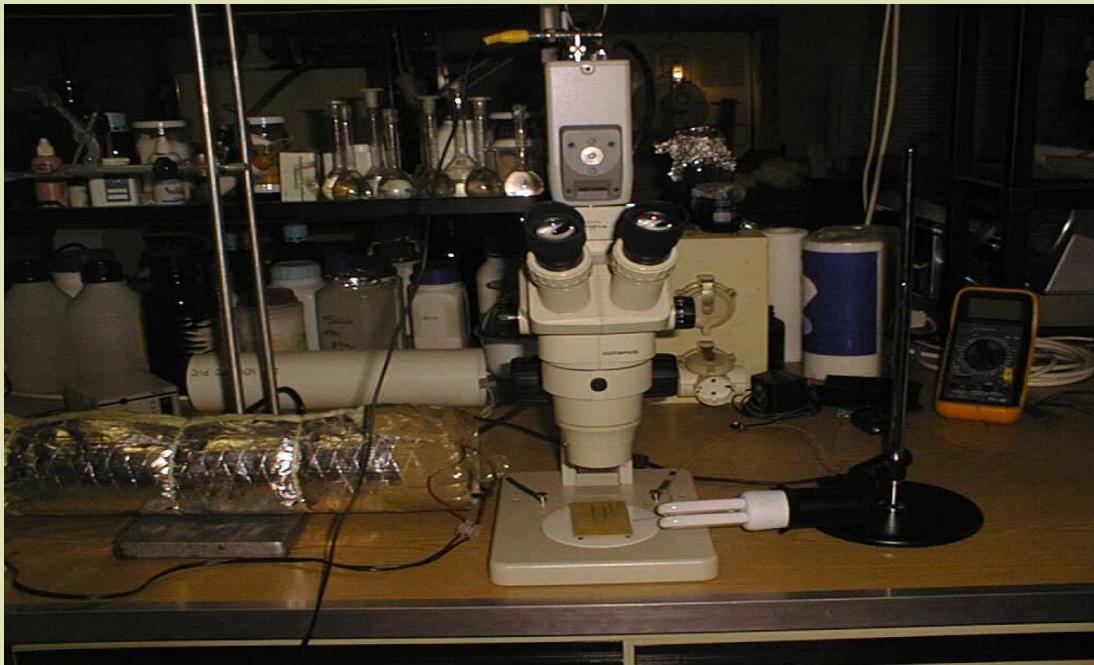
Less from cytoplasm and cellular walls



Microscopic Shrinkage

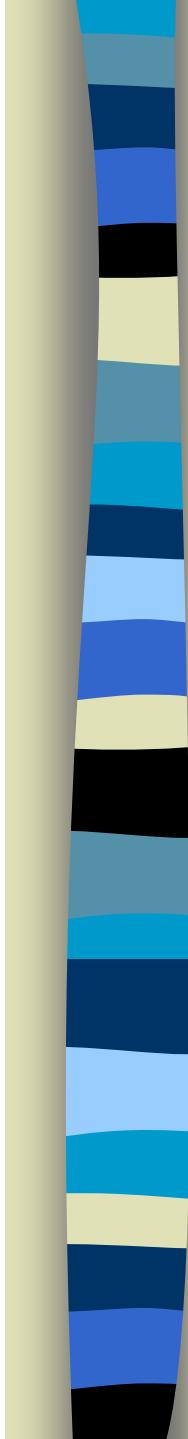


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Stero-microscope with video camera and air-drying tube.

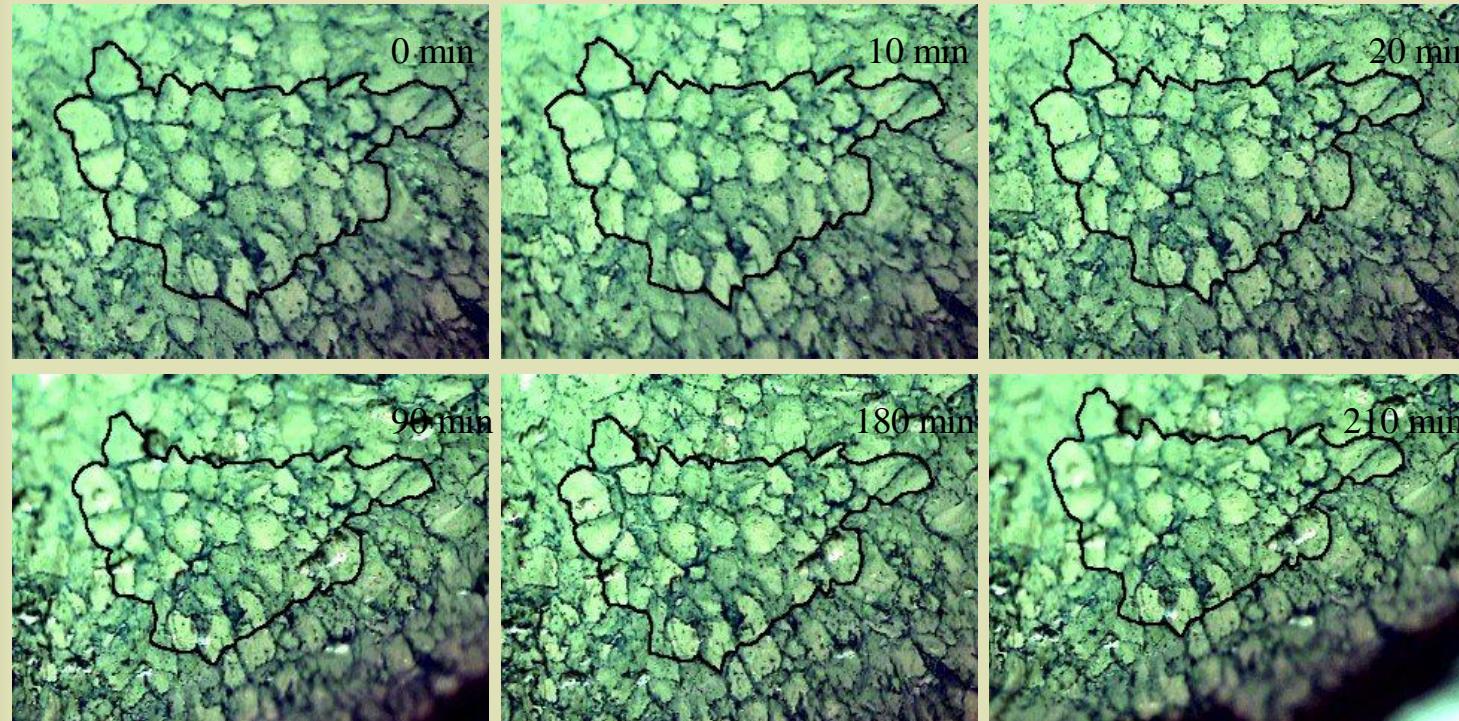
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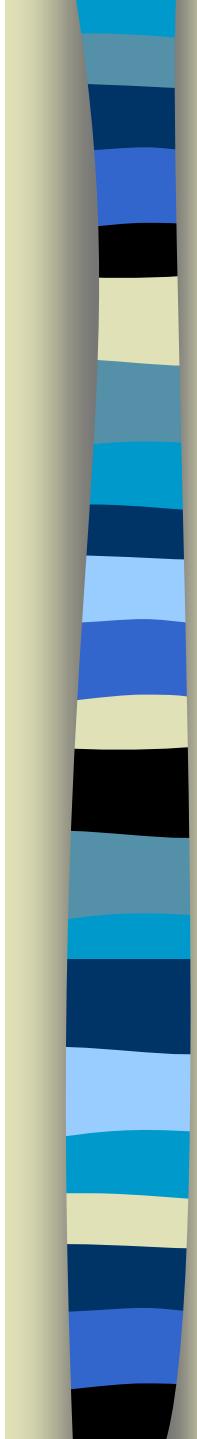
Microscopic Shrinkage



Cellular geometric features quantified by **image analysis**



Images of grape cells shrinkage at 40° C as a function of time.



Microscopic Shrinkage



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◆ Parameters:

➤ Dimensional: **area, perimeter,**

➤ **major and minor axis length**

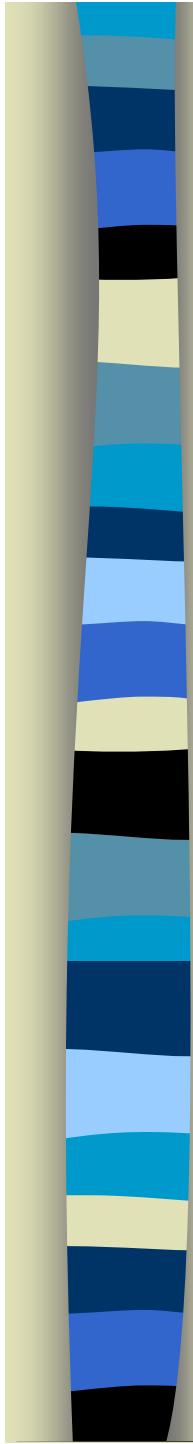
$$\text{Feret diameter } FD = 2 \sqrt{\frac{\text{area}}{\pi}}$$

➤ Shape:

$$\text{elongation} = \frac{\text{major axis length}}{\text{minor axis length}}$$

$$\text{roundness} = \frac{4\pi \text{ area}}{\text{perimeter}^2}$$

$$\text{compactness} = \frac{FD}{\text{major axis length}}$$

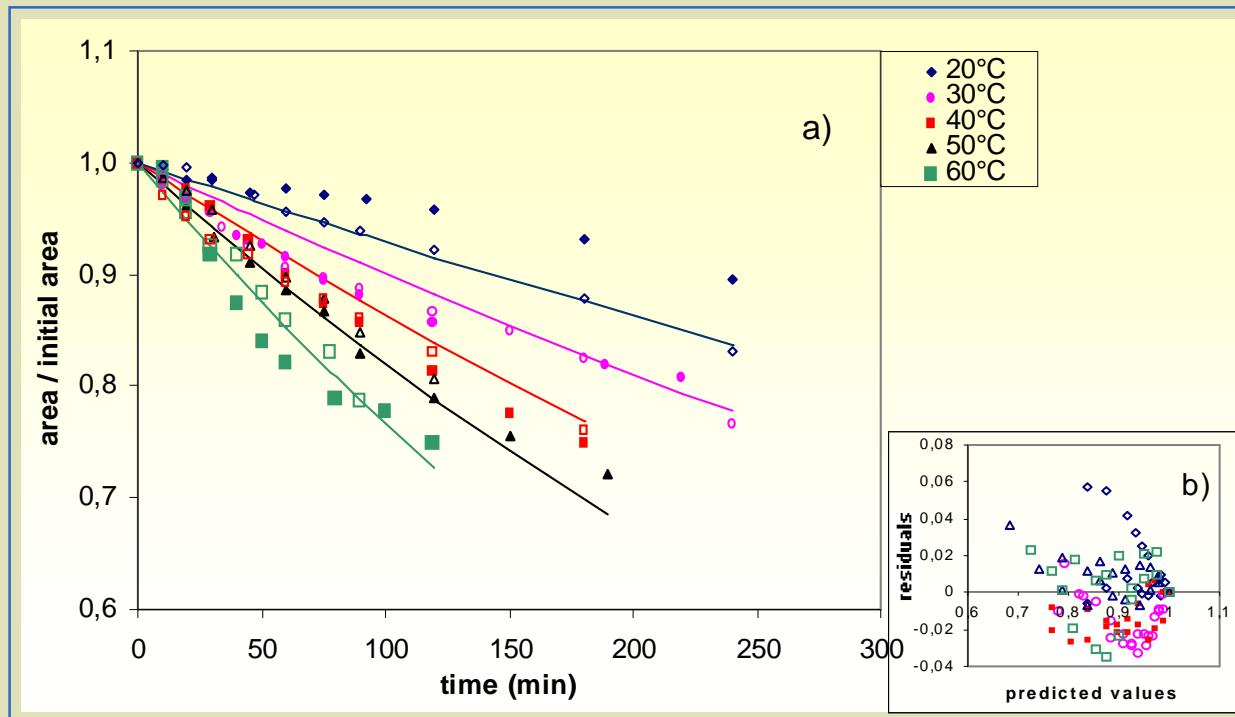


Microscopic Shrinkage

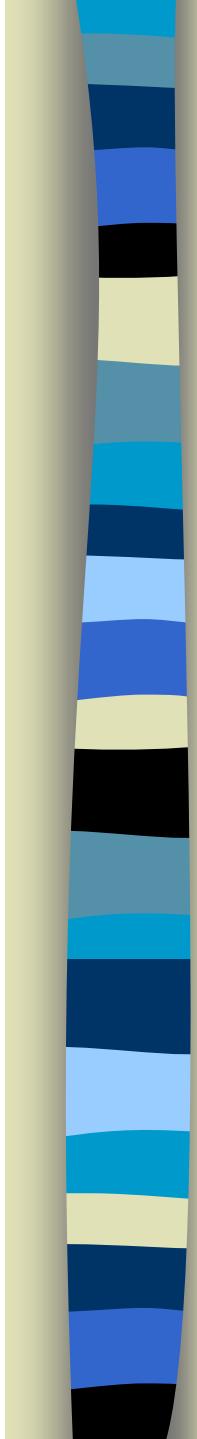


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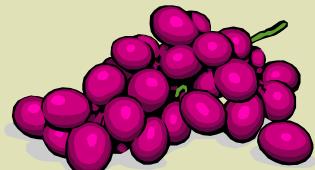
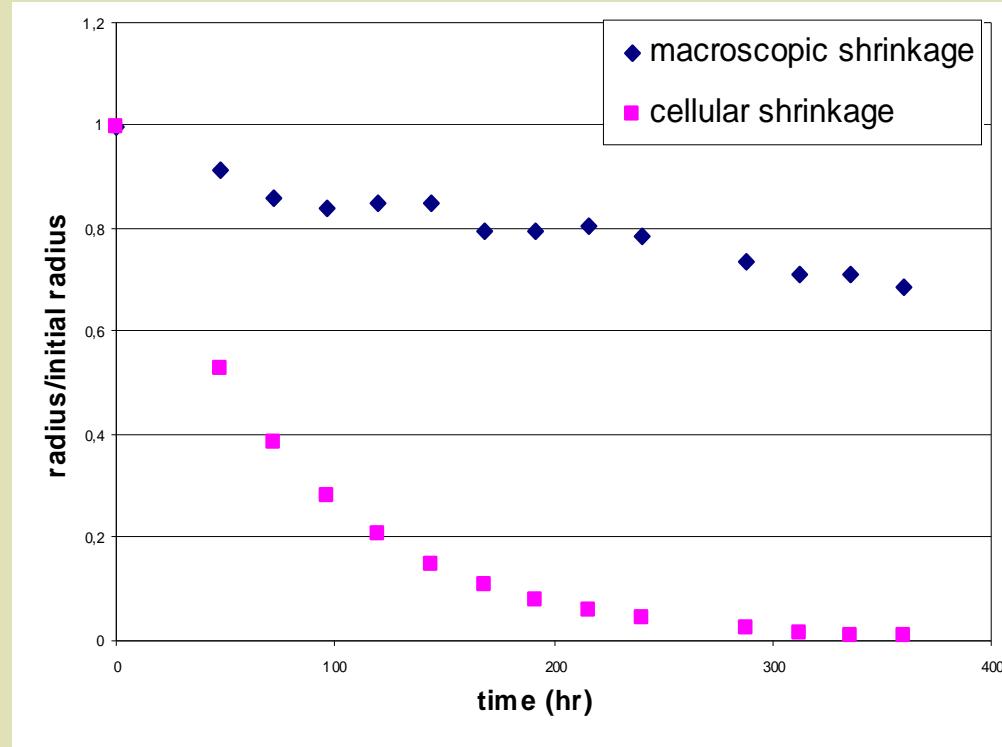
$$\frac{r}{r_0} = \exp \left\{ -K_{ref} \exp \left[-\frac{Ea}{R} \left(\frac{1}{T} - \frac{1}{T_{ref}} \right) \right] t \right\}$$



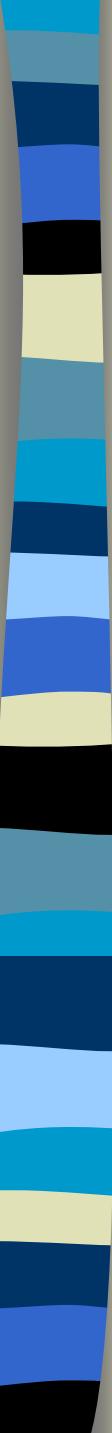
Relate Macroscopic and Microscopic Shrinkage



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Final Remarks

- Develop the mathematical basis and considerations for integrating heat and mass transfer phenomena.
 - include variable diffusivity
 - sorption isotherms
 - shrinkage

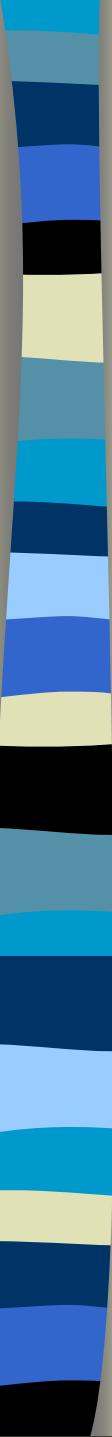




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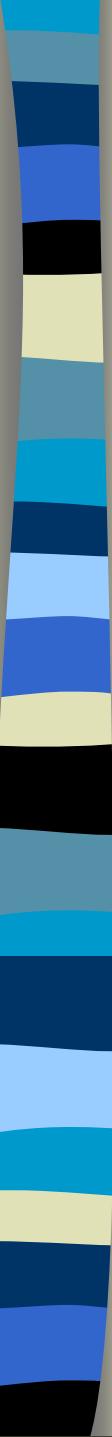




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 - include variable diffusivity
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- Lack of data on thermal properties of foods.
- Microstructure helps understanding drying mechanisms.
- Correlating microstructure, texture measurements and sensory analysis is an attractive area.

Acknowledgments



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Praxis XXI BD/18543/98



CYTED XI.13 "Relaciones Estructura -
Propiedad en la Deshidratacion y
Almacenaje de Alimentos Dehidratados"



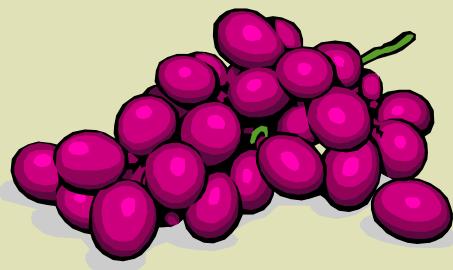
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Thank you



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