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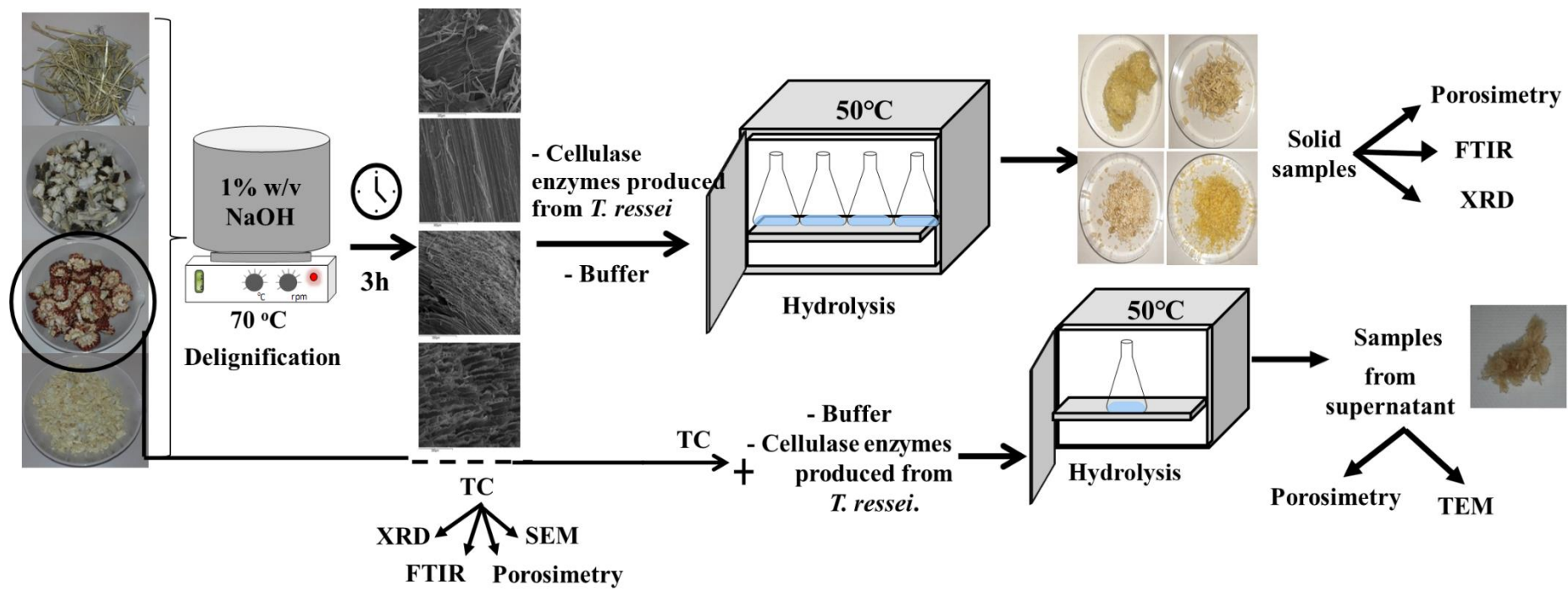
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Carbohydrate Nano-tubes Production and its Techno-economic Validation

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Abstract:	The production of carbohydrate nanotubes (CHNTs) using agricultural wastes is proposed in this investigation. The corn cob was found to be the most productive for our purpose among the four lignocellulosic raw materials tested. CHNTs production was accomplished in two stages. Tubular cellulose (TC) was prepared from raw substrates through a delignification process, and the prepared tubes of TC were cut into nano-size carbohydrate tubes in a chemical-free process. To achieve this, cellulase was produced in our lab using agricultural residue, employing the non-pathogenic fungus <i>Trichoderma reesei</i> , a high cellulase producer. Analysis of the produced CHNTs proved stability, nano-dimension lengths, and increased crystallinity. The techno-economic feasibility report showed that the production of CHNTs is cost-effective. This was supported by a process flow sheet with mass and energy balances based on laboratory experimental results.



Highlights

- Corncob treatment provide a cellulosic material with nanotubes
- The surface characteristics of corncob favored the formation of nanotubes
- CHNTs were present in the supernatant of the hydrolysis suspension
- Technoeconomic-feasibility report validated a cost-effective CHNTs production

1 **Carbohydrate Nanotubes Production and its Techno-economic Validation**

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11

12 **ABSTRACT**

13 The production of carbohydrate nanotubes (CHNTs) using agricultural wastes is proposed in
14 this investigation. The corncob was found to be the most productive for our purpose among
15 the four lignocellulosic raw materials tested. CHNTs production was accomplished in two
16 stages. Tubular cellulose (TC) was prepared from raw substrates through a delignification
17 process, and the prepared tubes of TC were cut into nano-size carbohydrate tubes in a chemi-
18 cal-free process. To achieve this, cellulase was produced in our lab using agricultural residue,
19 employing the non-pathogenic fungus *Trichoderma reesei*, a high cellulase producer. Analy-
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21 linity. The technoeconomic feasibility report showed that the production of CHNTs is cost-
22 effective. This was supported by a process flow sheet with mass and energy balances based on
23 laboratory experimental results.

24 **KEYWORDS:** *corncob; cellulose; Trichoderma reesei; cellulase; hydrolysis; Carbohydrate*
25 *nanotubes.*

26

27

28 1. Introduction

29 Over the past few decades, nanotechnology, nano-synthetic materials, and their applications have
30 gained attention. Carbon nanotubes (CNTs) are among the most commonly used nanomaterials. These
31 CNTs are rolled graphene with sp^2 hybridization and can be divided into three categories, according to
32 the number of tubes present in CNTs: single-walled CNTs, double-walled CNTs, and multi-walled
33 CNTs (Eatemadi et al., 2014; Ibrahim, 2013). Information on CNTs was first published in 1991
34 (Lijima, 1991), and since then this nanomaterial has established rapidly growing applications in sen-
35 sors, nanomedicine, environment, energy, and others (Ibrahim, 2013). However, their use in the bio-
36 logical and biomedical sectors of the human system is restricted due to their increased toxicity to the
37 human body. The size of nanotubes can affect the toxicity of CNTs, particularly those with a size un-
38 der 100 nm. They can affect the lungs and whole respiratory system by activating immunological re-
39 sponses modifying protein structure, and these re-disperse from their site of deposition in the human
40 system (Eatemadi et al., 2014; Satishkumar et al., 2000). Prolonged and excessive exposure to CNTs
41 can cause inflammation and oxidative stress (Nemmar et al., 2001).

42 In order to avoid the side effects of CNT use, we anticipated that alternative agricultural materials
43 could be used for nanotubes production. Inexpensive and renewable natural resources were explored
44 for the production of carbohydrate nanotubes (CHNTs). Such materials can be made from residual
45 plant stalks, which are generated as by-products of each crop. Globally, enormous amounts of agricul-
46 tural waste, such as wheat straw, sunflower stems, and corncobs, are produced each year following the
47 harvesting of wheat grains, corn, and sunflower seeds. (Barouni et al., 2015; Bian et al., 2018; Cavali
48 et al., 2020; Chen et al., 2021; FAO, 2019; Koutinas et al., 2016a; USDA, 2021). Nanofibers produced
49 from natural cellulosic waste materials and their application in nanocomposite materials are topics in
50 Green Advance. The advantages of cellulose nanofibers include their biodegradability, biocompatibil-
51 ity, renewable nature, high strength and stiffness, and low weight. (Kumar et al., 2020; Reddy and
52 Rhim, 2014; Sosiati et al., 2014). Furthermore, nanocellulose's structure can be modified to meet the
53 needs of particular applications by not only using a particular agricultural product as the material's ini-
54 tial carbon source but also by improving or changing the method of production. Nanocelluloses have

55 proven to be possible fillers for the improvement of the mechanical properties of biopolymer films,
56 such as starch, alginate, and chitosan films (Barouni et al., 2015; Koutinas et al., 2016a; Kumar et al.,
57 2020; Reddy and Rhim, 2014; Shankar and Rhim, 2016). Our previous studies have shown that ligno-
58 cellulosic material after delignification can be used for the formation of tubular cellulose with micro
59 and nano dimensions (Koutinas et al., 2016b). The aim of this work was the production of carbohy-
60 drate nanotubes (CHNTs), a new generation of nanotubes, from the carbon content of agricultural resi-
61 dues via the preparation of tubular cellulose (TC) in an enzymatic process.

62 2. Experimental

63 2.1 Agricultural residual materials

64 In our experiments, we used free or low-cost materials such as corncob and sunflower stems from lo-
65 cal farms, wheat straw from a local cattle feed market, and sawdust from a local timber mill.

66 2.2 Cellulase preparation

67 For a green, economical technology, we used cellulolytic enzymes prepared in our lab from carbon
68 sources of agricultural origin. A high cellulase-producer, *Trichoderma reesei* (ATCC 26921), was
69 grown on Potato Dextrose Agar (PDA) medium at 30 °C for 5-7 days. Fungal spores were aseptically
70 collected from the surface of PDA plates by gently scraping with sterilized water and were counted on
71 a hemocytometer (Neubauer Improved, HBG, Germany). The production of cellulase was carried out
72 using a modified method by Li et al. (2013). Two mL of spore suspension containing 10^6 - 10^7 spores
73 mL^{-1} was precultured in 60 mL of sterilized medium consisting of 2% w/v delignified sawdust, 1% soy
74 peptone, and 1% glucose. The pH of the medium was adjusted to 4.5 with a 2M NaOH solution and
75 incubated in a VELP Scientifica FOC incubator at 30 °C and 180 rpm for 24 h. Forty mL of freshly
76 grown preculture was aseptically added into a 2 L bioreactor (Electrolab), containing 1 L of sterilized
77 medium made of 25 g delignified sawdust, 1.7% soy peptone, 0.5% $(\text{NH}_4)_2\text{SO}_4$, 0.6% KH_2PO_4 , 0.2%
78 $\text{MgSO}_4 \cdot 7\text{H}_2\text{O}$, 0.25% glycerol, and 2 mL Tween 20. The bioreactor equipped with the control devices
79 Fermac 231/260 was operated at 26 °C, 300 rpm, 1.5 L/min ventilation and pH 4.5–5.0. After 150 h of

80 fungal growth, the content was aseptically centrifuged to obtain a clear supernatant for use as a crude
81 preparation of cellulolytic enzyme.

82 2.3 Assay of cellulase activity

83 One mL of crude enzyme (prepared as above) was mixed with 100 mL of sodium citrate buffer (pH
84 5.0). From this, 5 mL was placed in a 50 mL conical flask with 10 mL of buffer and 0.5 g of finely
85 stripped Whatman filter paper. The reaction mixture was incubated at 50 °C for 60 min, and the re-
86 leased glucose due to enzyme activity was measured by High Performance Liquid Chromatography
87 (HPLC) on a Shimadzu LC-9A. Enzyme units were calculated against a standard curve plotted for glu-
88 cose released in a similar reaction conducted with a commercial cellulase with known units (Chu et al.,
89 2012).

90 2.4 Stage-1 Preparation of tubular cellulose (TC)

91 Lignocellulosic materials, including corncob, sunflower stem, wheat straw, and sawdust, were sub-
92 jected to a very mild (1%, w/v) NaOH solution treatment for three hours at 70 °C. Materials were fil-
93 tered out and washed with hot (90 °C -95 °C) deionized water for complete removal of NaOH and re-
94 leased lignin. The delignified material produced in this procedure was employed as TC in a later stage;
95 therefore, it was freeze-dried at 15×10^{-3} mbar and -45 °C using a Labtech Daihan Freeze Dry System.

96 2.5 Stage-2 Enzymatic treatment of TC to develop CHNTs

97 In separate flasks containing 200 mL of buffer pH 5.0 and 10 mL of crude enzyme, 15 g of TC pre-
98 pared from four agricultural residues were incubated at 50 °C for 72 hours without stirring or mixing.
99 To examine the formation of CHNTs samples from the flasks of each substrate were taken at 5, 24, 48,
100 and 72 h intervals.

101 2.6 Stage-3 Isolation of CHNTs

102 After hydrolysis of TC a quantity of clear supernatant liquid without dispersed solids was taken in or-
103 der to isolate the water-soluble CHNTs. The liquid was freeze-dried, and porosimetry and TEM analy-
104 sis were performed in the powder received.

105 2.7 Examination of CHNTs

106 Following all Standard Operating Procedures (SOPs) for each equipment used, examination of CHNTs
107 was conducted as below: Specific surface area, pore size distribution, and pore volume of all types of
108 materials (original raw material, TC, and CHNT) was carried out by N₂ adsorption-desorption process
109 at -196.15 °C on a Tristar 3000 porosimeter (Micromeritics); Jeol Model JSM-5600LV scanning elec-
110 tron microscope was used operating at an accelerating voltage of 20 kV; X-ray powder diffractometry
111 (XRD) was used to test the crystallinity of materials on a Bruker AXS D8 ADVANCE at 40 kV and 20
112 mA. Segal's equation based on the diffraction pattern intensity was used for the calculation of the
113 crystallinity index (CI). Transmission Electron Microscopy (TEM) images were taken with the help of
114 a Gatan model 782 Erlangshen E5500W camera. FTIR spectra of samples were obtained using a FTIR
115 Perkin-Elmer spectrophotometer, 16 PC model, in the range of 4000–400 cm⁻¹.

116 2.8 Technoeconomic validation and Process Flow Sheet for industrial application

117 Details of the process flow sheet design are presented in Figure 5, and the investment and daily pro-
118 duction costs are presented in Tables 4 and 5, respectively. The delignification of biomass takes place
119 in tank 1, by supplying steam through a boiler (11) and the delignified cellulosic material is transferred
120 to enzyme production bioreactor (2) and CHNT production bioreactor (5). The enzyme production bio-
121 reactor (2) is supplied with air by an air pump (4) through a sterile filter (3). The temperature in biore-
122 actors 2 and 5 is kept constant at 26 °C and 50 °C respectively, by supplying steam from the boiler (11).
123 The hydrolysate from the bioreactor 5 containing CHNTs is pumped to the centrifugal separator (7) to
124 separate suspended solids from the solution of CHNTs. A clear CHNTs solution is collected in tank 8,
125 then concentrated in a condenser (9), and subsequently freeze-dried in a freeze-dryer system (10).

126

127 3. Results and Discussion

128 3.1 Structure of TC

129 From the SEM images (Fig. S1) of wheat straw, sunflower stem, corncob, and sawdust (original and
130 delignified), it can be observed that the morphology of the materials changed after delignification,
131 pores were created on the surface of the materials, and the fibers arranged in TC could be seen (Fig.
132 S1) These changes are attributed to the removal of amorphous areas, which was earlier occupied by lig-
133 nin and hemicellulose contents in raw substrates (Cavali et al., 2020). The two naturally occurring
134 forms of cellulose are $I\alpha$ and $I\beta$. In this analysis, only $I\beta$ was visible, as it is part of higher plants, in
135 contrast to the form $I\alpha$ only found in bacterial and algae celluloses (Poletto et al., 2014). Studies of
136 atomic resolution synchrotron and neutron diffraction data, have shown that cellulose $I\alpha$ has a triclinic
137 unit cell P1 ($a = 6.717 \text{ \AA}$, $b = 5.9962 \text{ \AA}$, $c = 10.400 \text{ \AA}$, $\alpha = 118.08^\circ$, $\beta = 114.80^\circ$, and $\gamma = 80.37^\circ$) con-
138 taining a single cellulose chain, while cellulose $I\beta$ has a monoclinic unit cell P21 ($a = 7.784 \text{ \AA}$,
139 $b = 8.201 \text{ \AA}$, $c = 10.380 \text{ \AA}$, $\alpha = \beta = 90^\circ$, $\gamma = 96.5^\circ$) containing two conformationally distinct cellulose
140 chains, called original chains and central chain (Krichen et al., 2022). The structure of cellulose $I\beta$ is
141 mainly in the form of parallel chains linked by H-bonds stacked with an alternating shear parallel to
142 the chain axis stabilized by Van der Waals interactions (Poletto et al., 2014). After delignification of
143 materials, the specific surface area of TC (Table 1) was about 2-fold higher due to the formation of
144 cellulose tubes in the space created by the removal of lignin fraction. The pore volume and pore size
145 were also increased, except for TC prepared from sunflower stem, which had a lower specific surface
146 area (Table 1).

147 3.2 Crystallinity analysis

148 The degree of cellulose crystallinity plays an important role in cellulose structure parameters. Since
149 the crystal structure of cellulose affects the enzymatic hydrolysis (Park et al., 2010), the crystallinity
150 was examined in XRD analysis (Fig. 1 and Table 2). The characteristic peaks of $I\beta$ cellulose were ob-
151 served at 2θ (theta) of about 16° , and 22.64° (Banvillet et al., 2021; Bian et al., 2018; Ling et al., 2021;
152 Zhang et al., 2021). The sharper peaks in the XRD profile of TC materials indicate that their degree of
153 crystallinity was higher compared to that of the raw materials. For delignified sawdust, sunflower
154 stem, and wheat straw, a peak located at 2θ of about 30.0° was also identified. This can be an indica-
155 tion of amorphous areas after delignification (Sosiati et al., 2015; Sosiati and Harsojo, 2014). Another

156 characteristic peak of cellulose I β at 2θ of about 35.0° appeared for all materials (Banvillet et al.,
157 2021; Ling et al., 2021; Zhang et al., 2021). An increase in the rigidity of cellulose tubes (fibers) and a
158 decrease in their flexibility occur when there is an increase in the ratio of crystalline to amorphous re-
159 gions. Sunflower stem and corn cob had the lowest crystallinity indices (CI) (Table 2). CI increases as
160 the surface area of the crystallites corresponds to decrease in amorphous cellulose, due to the void
161 spaces available after lignin removal (Cavali et al., 2020; Poletto et al., 2014).

162 3.3 FT-IR spectra

163 The spectra for corncob and wheat-straw are presented in Figs. 2a and 2b, for the other two materials,
164 spectra were similar (hence not presented here). At around $3440\text{-}3420\text{ cm}^{-1}$ an intramolecular H-bond
165 vibration appeared, which indicates cellulose (Poletto et al., 2014). The FTIR absorption peaks at
166 $\sim 2900\text{ cm}^{-1}$ are characteristic of the stretching vibration of C-H groups of cellulose (Reddy and Rhim,
167 2014). The absorption peaks at $1440\text{-}1430\text{ cm}^{-1}$ are due to CH_2 bending vibration and indicate the
168 “crystallinity band” in the cellulose. A reduction or expansion in the intensity of this crystallinity band
169 among the untreated, delignified freeze dried, and after enzymatic hydrolysis samples indicates that
170 the level of crystallinity of cellulose crystals decreased/increased during treatment processes (Shankar
171 and Rhim, 2016). The peaks appeared at 1375 cm^{-1} are typical of the O-H bending vibration of cellu-
172 lose. The peaks at $1163\text{-}1165\text{ cm}^{-1}$ are attributed to the C-O-C pyranose ring stretching vibration and
173 the peaks at $896\text{-}898\text{ cm}^{-1}$ indicate the C-H rocking vibration of cellulose present in the microfibers
174 and nanofibers (Reddy and Rhim, 2014). No considerable changes in the absorption peak positions of
175 untreated and delignified freeze-dried samples (TC), were observed (Figs. 2a and 2b), which indicated
176 that these processes did not alter the chemical structure of the cellulosic materials. However, the spec-
177 tra bands present at around 1730 cm^{-1} in raw lignocellulosic (due to C-O stretching vibration for the
178 acetyl and ester linkages in lignin/hemicellulose) were absent in the spectra of TC. That confirmed the
179 absence of lignin and hemicellulose in TC, which were removed in stage 1 of alkali treatment (Gabriel
180 et al., 2020; Kargarzadeh et al., 2012; Kumar et al., 2020).

181 3.4 Enzyme treatment of TC for development of CHNTs

182 TC materials were treated with our lab-prepared crude cellulase (70 FPU/g) to develop CHNTs. N₂ ad-
183 sorption-desorption porosimetry analysis (Figs. 3a, b, c) show the kinetics: BET surface area (m²/g) and
184 pore volume are given by BJH equation, and the pore size by BET (nm). CHNTs were produced after
185 24 h enzyme treatment of TC obtained from four agricultural substrates. CHNTs from corn cob pre-
186 sented the highest value of surface area (1.8 m²/g), which is a desired parameter for the entrapment of
187 pharmaceutical substances, food preservatives, and other entities in CHNTs (Panitsa et al., 2021).
188 Based on the number of tubes with pore widths between 2-70 nm (Fig. 3d) in combination with pore
189 volume (0.013 cm³/g) and the average pore diameter (13.5 nm), corncob-TC proved to be the most
190 productive material among the TC of other substrates, for the development of CHNTs.

191

192 *3.5 Physicochemical properties of the isolated CHNTs product*

193 CHNTs retain some important properties of cellulose, such as biodegradability and non-tox-
194 icity. CHNTs are oligomers with glucose as their structural unit and can form hydrogen bonds
195 with OH groups containing enzymes and drugs. The characterization of the isolated product
196 of CHNTs was carried out by TEM to prove the nanodimensions of the length of tubes. Po-
197 rosimetry analysis confirmed the pore size (Table 3) and pore distribution (Fig. S3), classify-
198 ing the material, a nanomaterial.

199 *3.5.1 Transmission Electron Microscopy of the isolated CHNTs product*

200 TEM images of CHNTs developed from corncob showed needle-like cellulosic nanotubes
201 (Fig. 4 a, b) with an internal diameter 6-16 nm and a length of tubes in the range of 80-160
202 nm. These data proved that the cellulosic tubes in TC after treatment with cellulolytic en-
203 zymes produced carbohydrate nanotubes (CHNTs).

204 *3.5.2 Porosimetry analysis of the isolated CHNTs product*

205 The BET surface area was 1.35 m²/g and the pore width was 4.6 nm after 72 hours of hydrol-
206 ysis, as shown in Table 3. Porosimetry measurement revealed an average pore diameter (tube
207 diameter) of around 4-5 nm (Fig. 4b), which is consistent with the size of the tubes depicted
208 in the TEM image.

209 *3.6 Design and operation of the bioreactor and economic validation of technology*

210 The bioreactor system presented in Figure 5 contains bioreactor 2 of 10,000 L for enzyme
211 production and bioreactor 5 of 100,000 L for tubular cellulose (TC) hydrolysis to nanotubes.
212 Machineries of high cost are the condenser (9), freeze dryer (10), and centrifugal separator
213 (7). The boiler (11) that produces 850 liters of oil per day and the delignification tank (1) are
214 also of importance. Delignification tanks (1) and condensers (9), respectively, need about 87%
215 of steam consumption. Centrifugal separators (7) and freeze dryers (10) need more than 90%
216 electricity consumption. The total investment cost has been calculated at €1,743,000, with the
217 biggest costs being those of the condenser (€300,000), freeze dryer (€500,000), and boiler
218 (€600,000). The parameters considered for the calculation of the daily production cost were
219 raw material cost, labor, thermal energy, electricity, water requirement, consumables, and in-
220 vestment payment costs. The biggest costs are the labor cost and that of thermal energy, which
221 are about 70% of the €2,731 daily cost. On the other hand, the annual turnover is equal to
222 about €1,500,000, which could give a profit of €300,000 annually. So, it is estimated that the
223 payment of investment costs will be achieved in about 6 years. This short period of invest-
224 ment repayment shows that the technology has a large margin of profit to convince the inves-
225 tors to proceed.

226 *3.7. Technological and scientific implications*

227 The aforementioned presentation of results and discussion have demonstrated the production
228 of CHNTs. Specifically, the XRD and FTIR analysis proved that the tubes consist of cellulose,

229 while lignin and hemicelluloses have been removed. They also proved the increment of crys-
230 tallinity indices, which is related to the rigidity of tubes. The formation of a new generation of
231 tubes could lead to the preparation of a carrier material potentially usable as a drug delivery
232 system. The metabolism and safety of CHNTs in the human body should be examined. Immo-
233 bilization of cellulase in CHNT tubes with pharmaceutical substances could be considered a
234 possible method for removing the carrier material from the body after its action. Cellulase has
235 the ability to hydrolyze cellulose into glucose, a nutrient for humans. Finally, the method of
236 producing CHNTs is feasible, and the raw material is sustainable. The technoeconomic valida-
237 tion based on laboratory results showed that the process is cost-effective. This is supported by
238 laboratory results (Table S1).

239

240 **4. Conclusions**

241 The Technoeconomic feasibility report validated that CHNT production is cost-effective. A green tech-
242 nology was applied for four agricultural residual materials. Among them, corncob has proved the most
243 productive. It is free, making our process economically viable. TC tubes from corncob were cut short
244 with cellulase, a cheaper lab preparation from *Trichoderma reesei*, to carbohydrate tubes of nano-size.
245 FTIR and XRD analysis revealed the stability of CHNT's chemical structure. CHNTs were isolated
246 from the solution of hydrolyzed cellulose after freeze-drying. The nano-dimension tubes of the final
247 product were confirmed by TEM and porosimetry analysis. CHNTs-based carrier materials could po-
248 tentially be used as drug delivery systems. However, their metabolism in the human body should be
249 studied for their safety.

250

251 E-supplementary data for this work can be found in e-version of this paper online

252 .

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267 The authors declare that they have no known competing financial interests or personal rela-
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269 **CRedit authorship contribution statement**

270 All authors contributed to the study conception and design. **Athanasia Panitsa:** Methodol-
271 ogy, Validation, Investigation, original draft, Visualization. **Theano Petsi:** Methodology,
272 Writing-review & editing. **Eleana Kordouli:** Methodology, Validation. **Poonam S. Nigam:**
273 Result-analysis for writing-second draft, editing. **Maria Kanellaki:** Supervision. **Athanasios**
274 **A. Koutinas:** Conceptualization, Writing-original draft, Project-administration, Funding-ac-
275 quisition. All authors read and approved the final manuscript.

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373 **Figure captions**

374 **Figure 1.** XRD spectra of (a) untreated and (b) delignified freeze dried cellulosic materials.

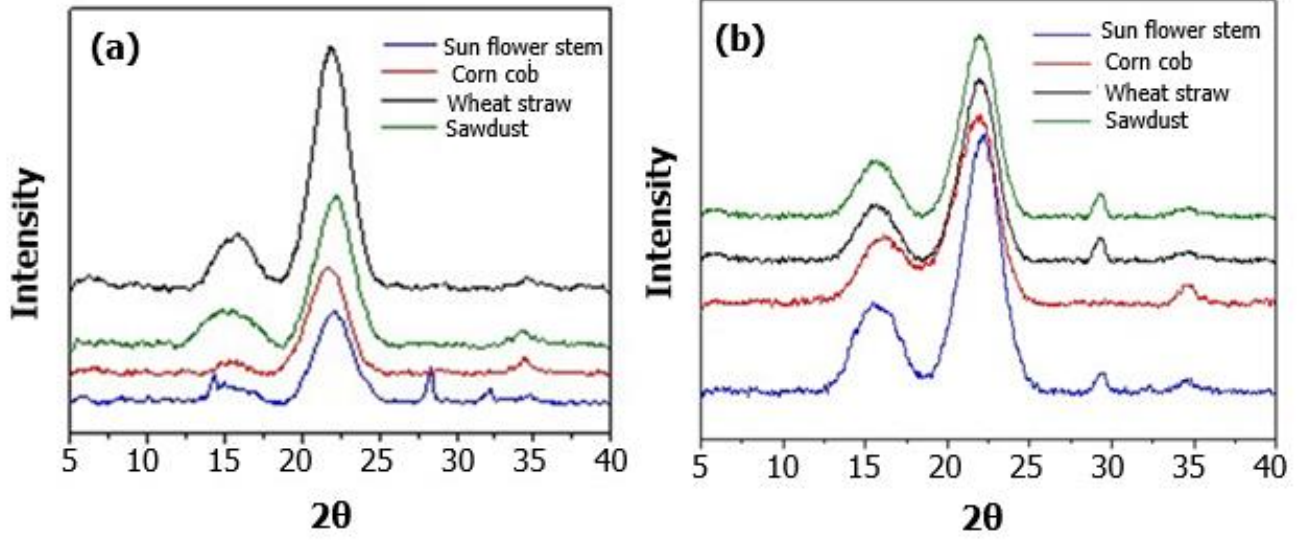
375 **Figure 2.** FTIR spectra of untreated (black), delignified freeze dried (blue) and after hydroly-
376 sis (red) (a) corn cob and (b) sawdust, (c) FTIR spectra of solid formed by freeze dried sam-
377 ples of the supernatant after: 24 h (black), 72 h (blue), 168 h (red) and 336 h (pink) of corn
378 cob's hydrolysis.

379 **Figure 3.** Porosimetry analysis of delignified cellulosic materials during their hydrolysis with
380 cellulase. (a) BET surface area (m^2/g), (b) Pore volume (BJH) (cm^3/g), (c) Pore size (BET)
381 (nm), (d) % pore volume between 2-70 nm of delignified freeze dried cellulosic materials dur-
382 ing their hydrolysis with cellulase enzymes.

383 **Figure 4.** (a) TEM image of hydrolyzed corn cob (solid part) after 24 h of hydrolysis, (b)
384 TEM image of solid formed by freeze-dried samples from supernatant after 72 h of corncob's
385 hydrolysis.

386 **Figure 5.** Process flow sheet with mass (kg) and energy (kg of steam) balance for CHNTs
387 production. 1. Delignification tank (100 m^3); 2. Enzyme production bioreactor (10 m^3); 3.
388 Sterile filter ($150 \text{ m}^3/\text{min}$); 4. Air pump ($150 \text{ m}^3/\text{min}$); 5. CHNTs production bioreactor (100
389 m^3/min); 6. Pump ($4 \text{ m}^3/\text{h}$); 7. Centrifugal separator ($20 \text{ m}^3/\text{h}$); 8. Tank for CHNTs solution
390 (100 m^3); 9. Condenser ($3.3 \text{ m}^3/\text{h}$); 10. Freeze dryer – water removal (6000 kg/d); 11. Boiler
391 (2500 kg oil/day); 12. Pump ($20 \text{ m}^3/\text{h}$); 13. Vacuum pump 5Hp

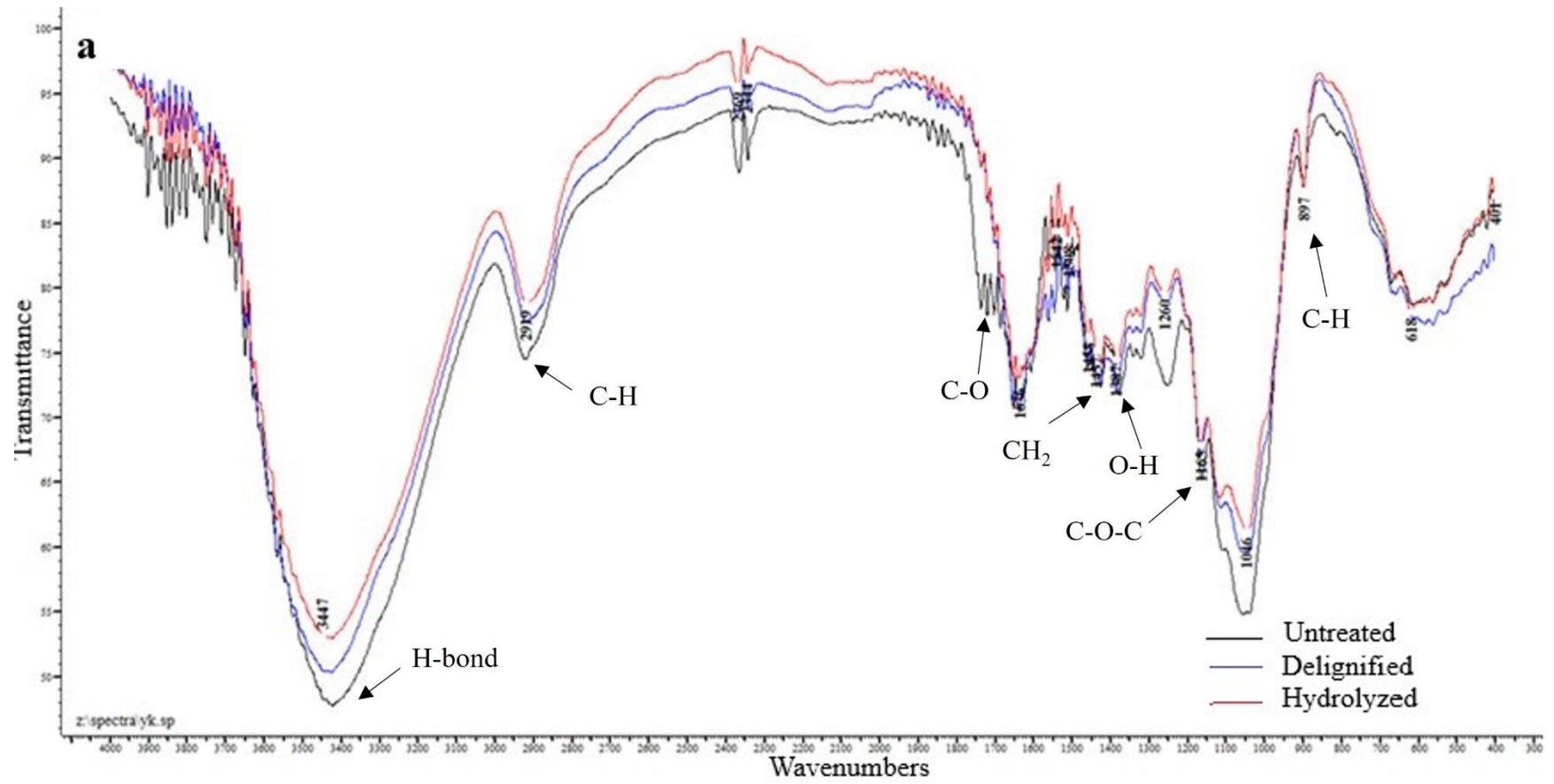
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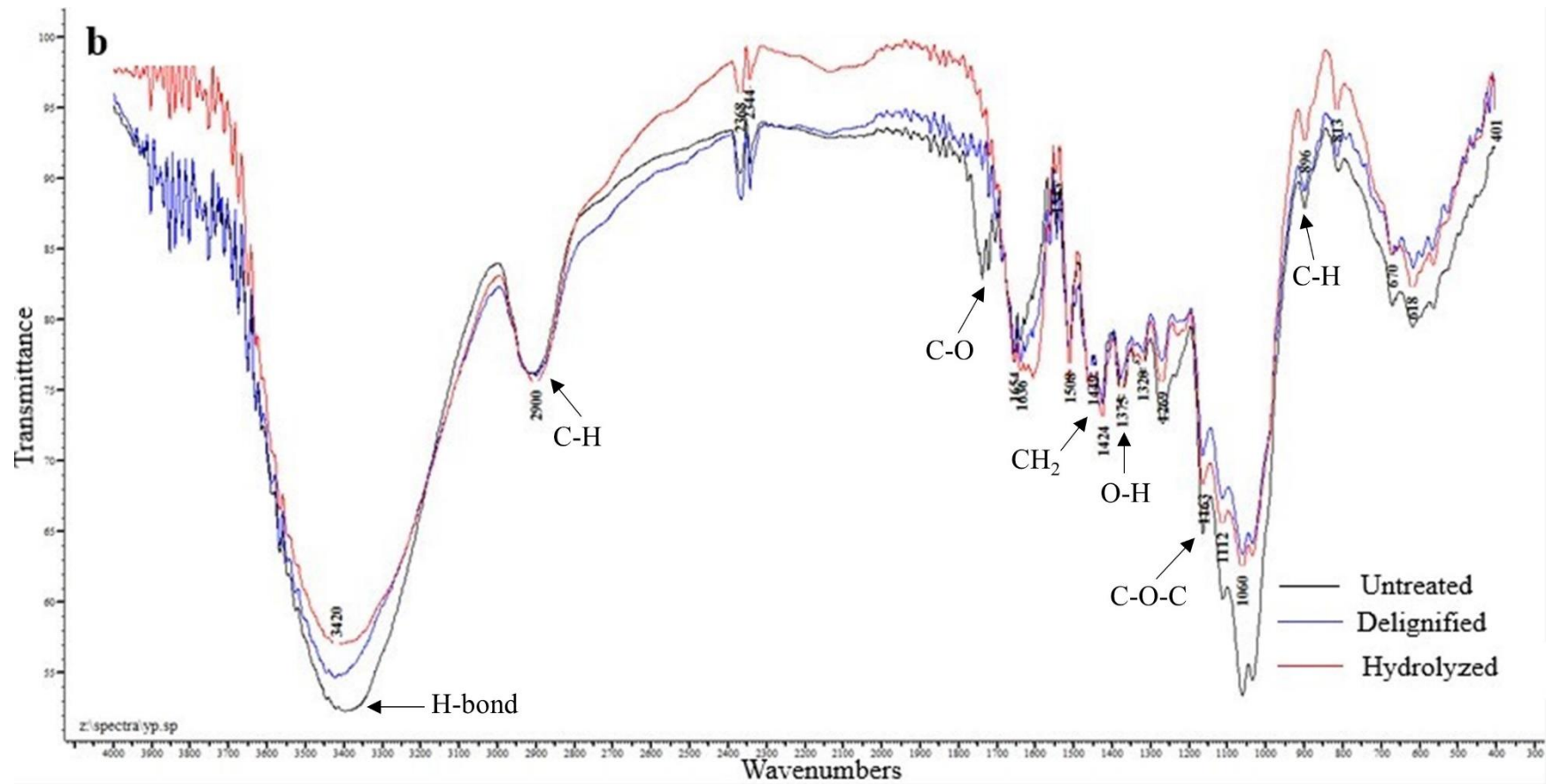
Figure 1.

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Figure 2a.



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Figure 2b.

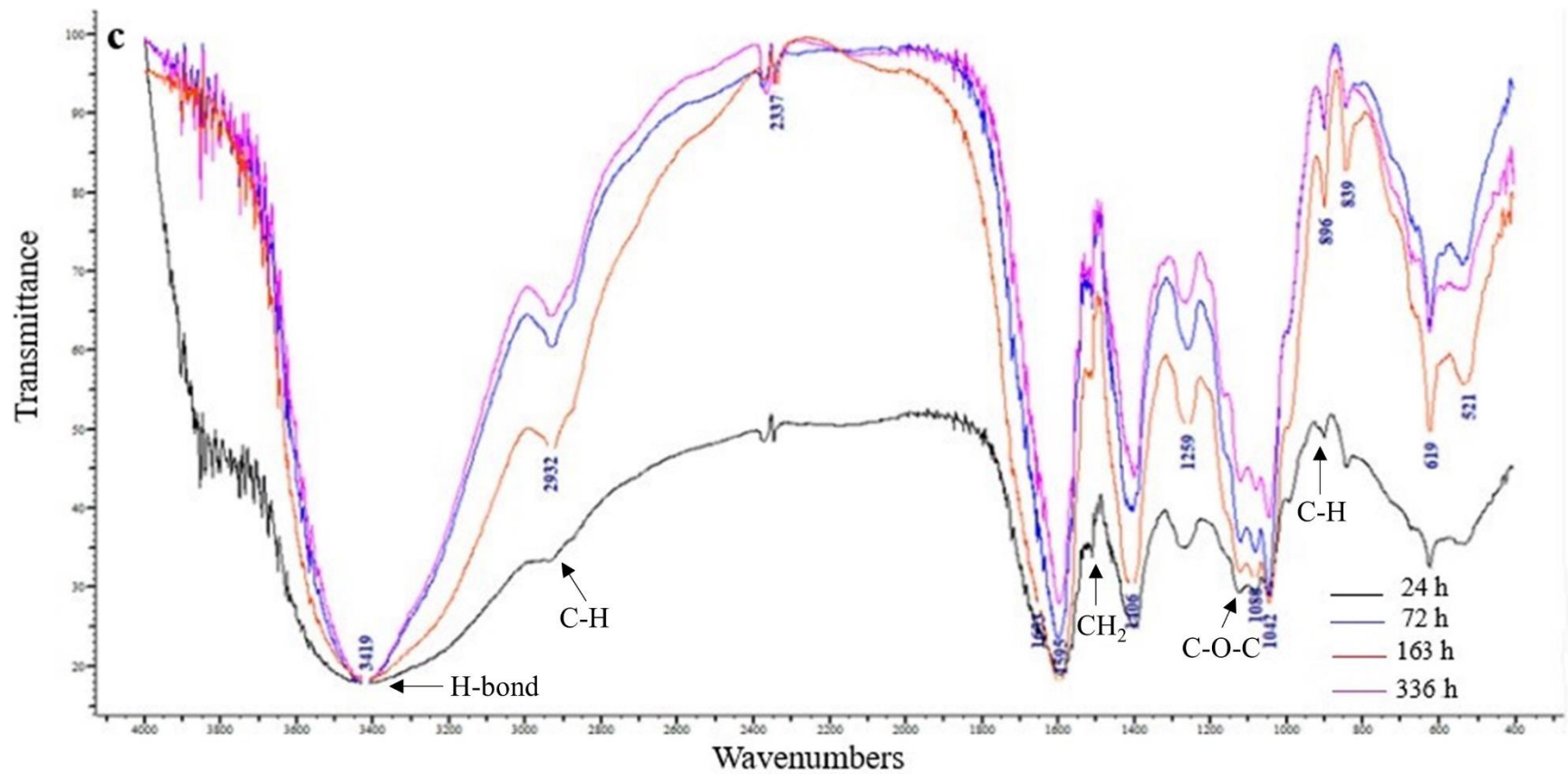


Figure 2c.

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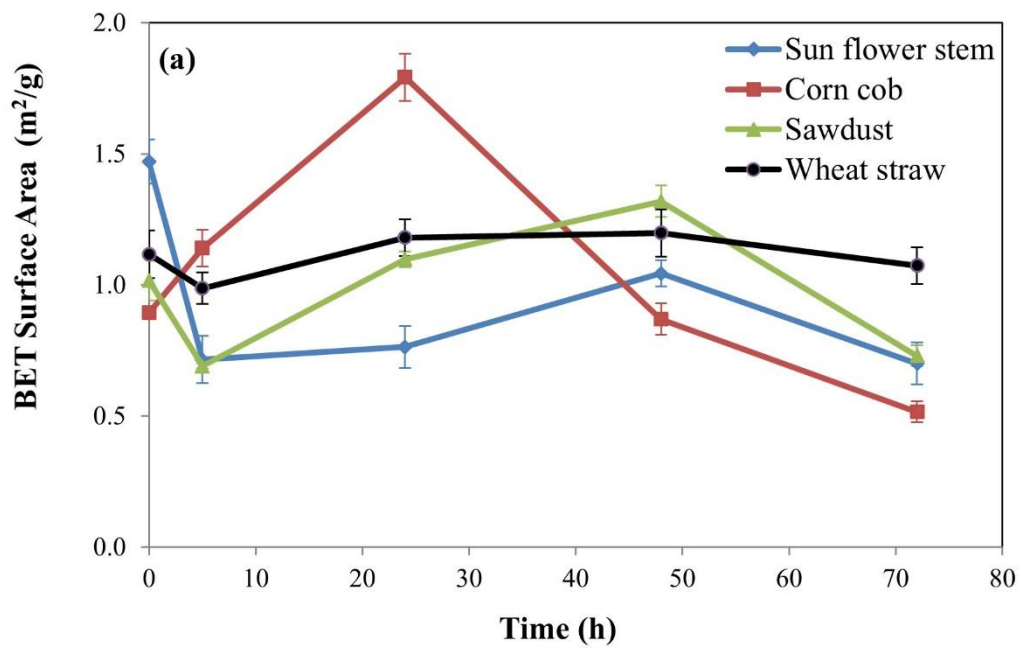


Figure 3a.

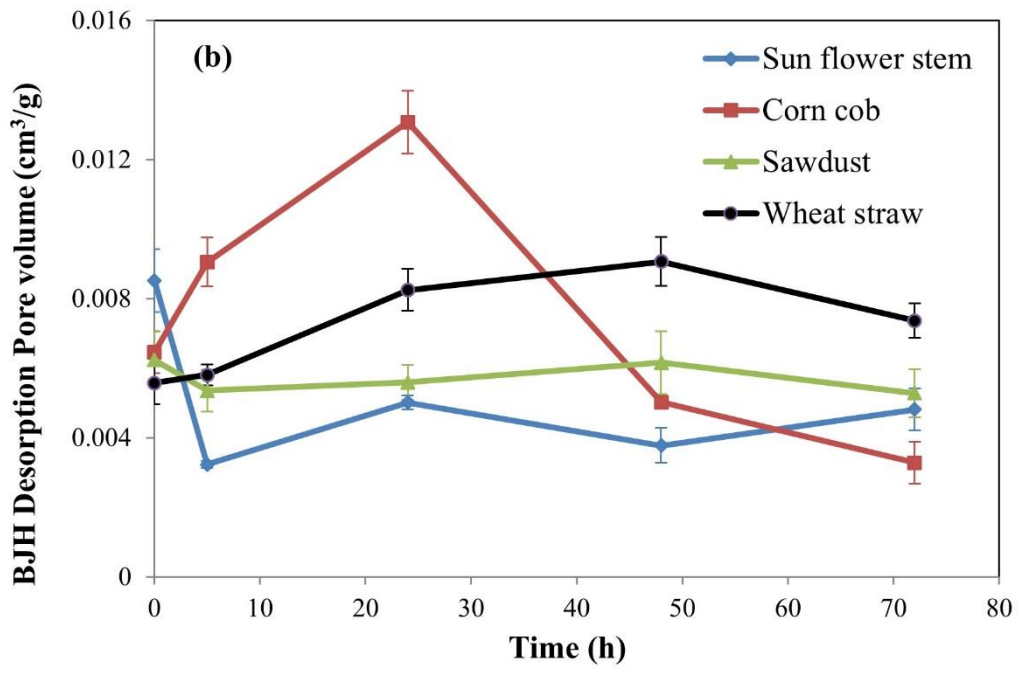


Figure 3b.

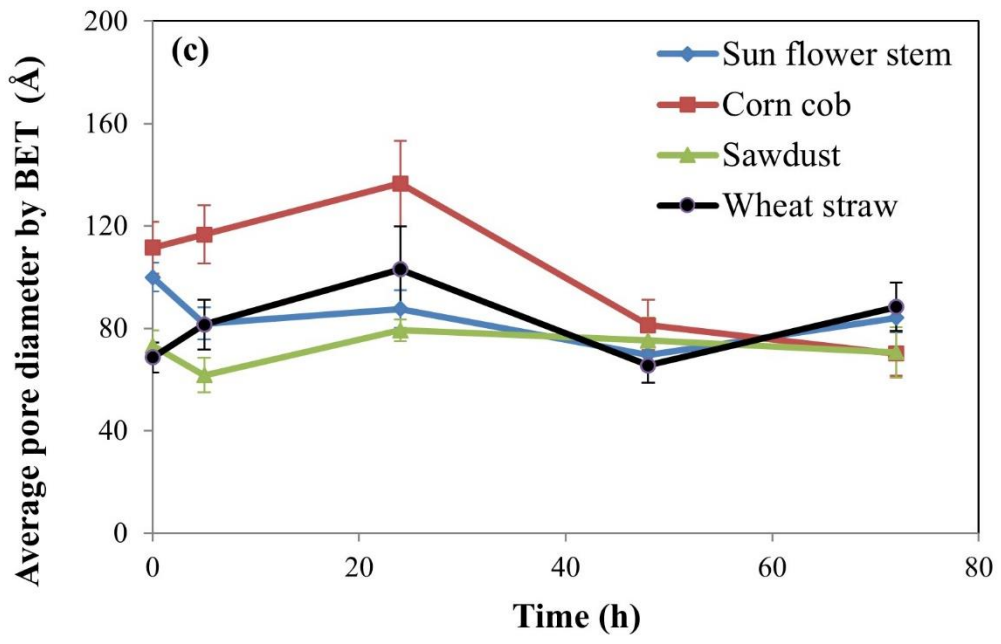


Figure 3c.

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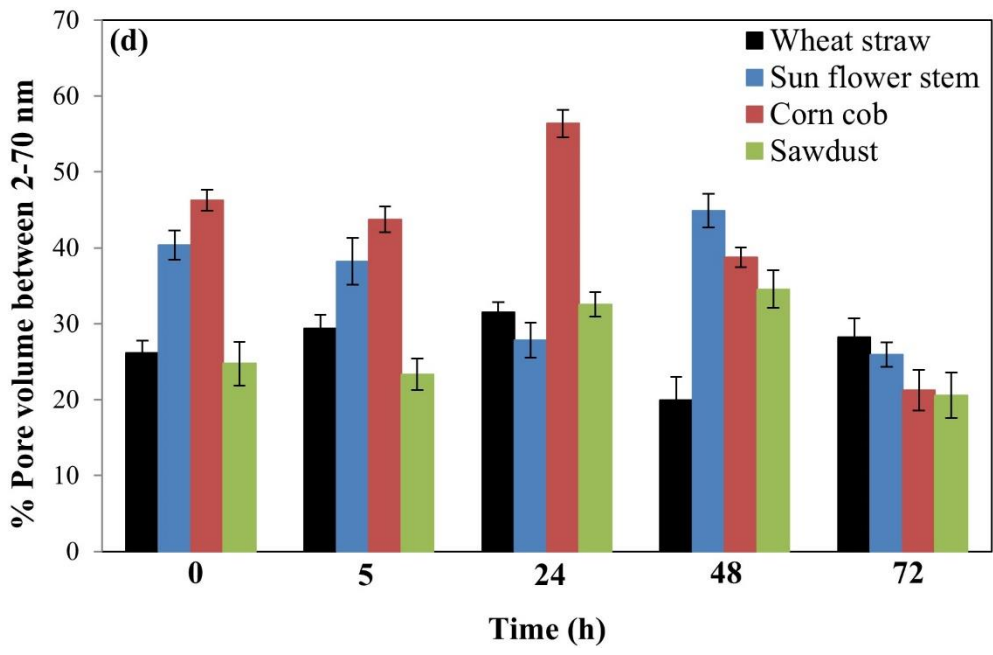


Figure 3d.

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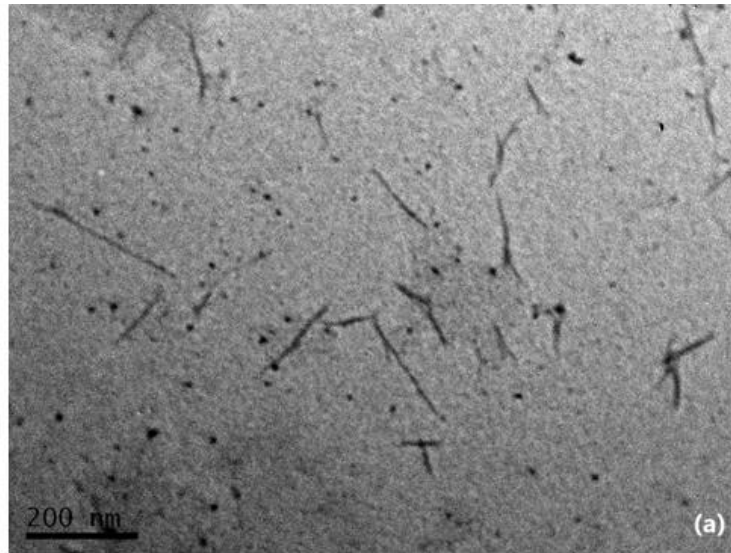
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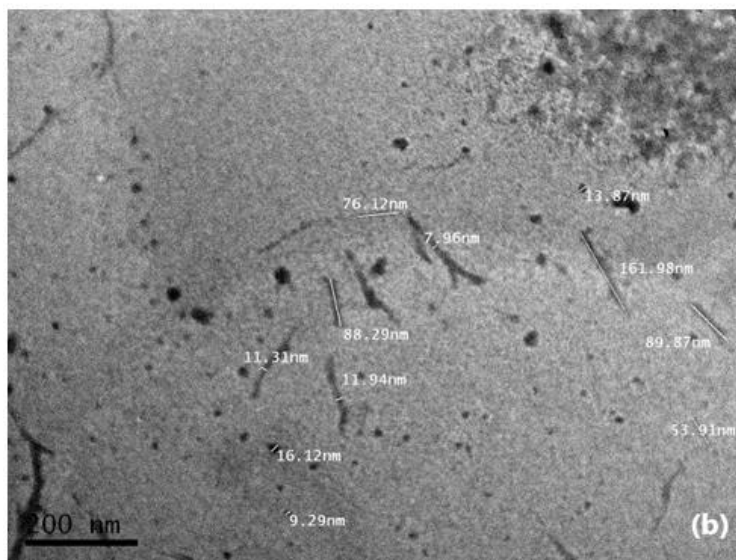
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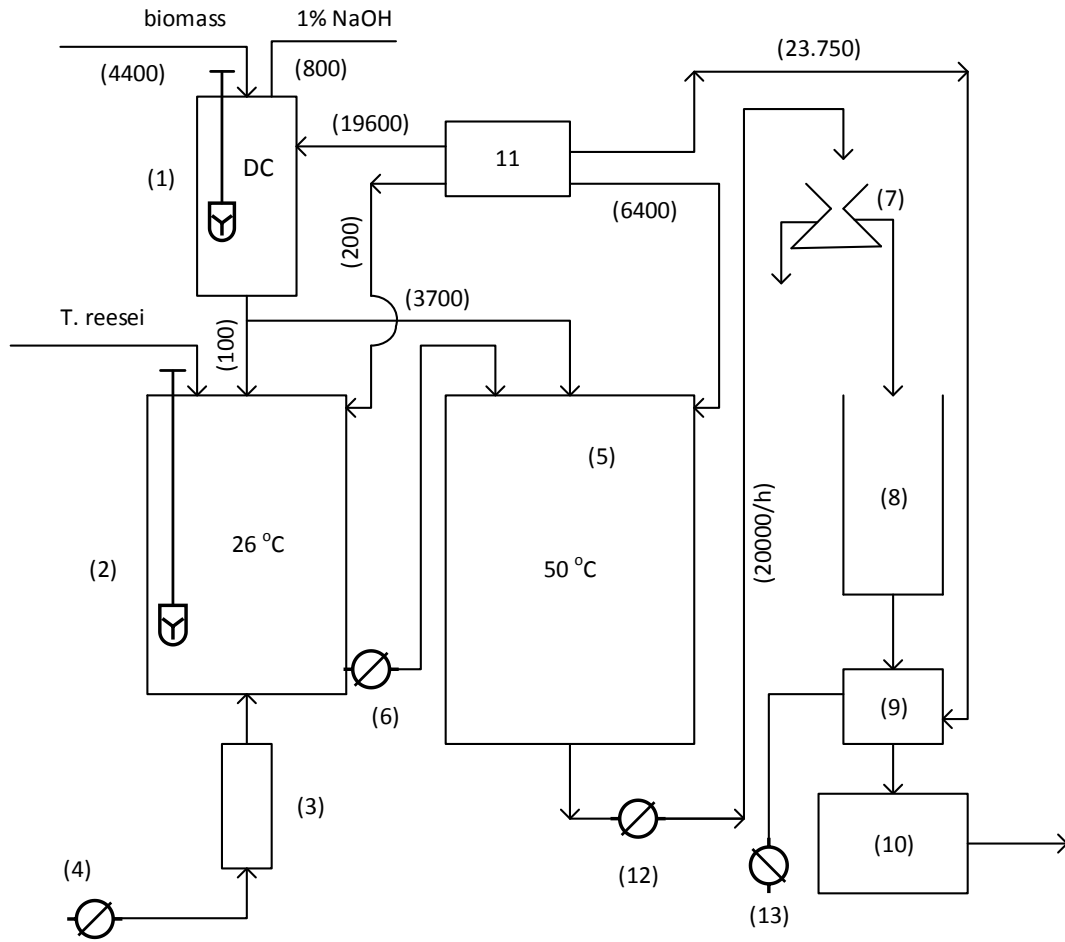
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Figure 4.

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Figure 5.

487 **Table 1.** Porosimetry analysis of untreated and delignified freeze dried (TC) cellulosic materi-
 488 als.
 489

Cellulosics	BET Surface area (m²/g)		Pore volume_(BJH) (cm³/g)		Pore size_(BET) (nm)	
	Untreated	TC	Untreated	TC	Untreated	TC
Wheat straw	0.48 ± 0.01	1.12 ± 0.09	0.0034 ± 0.0006	0.0056 ± 0.0006	8.23 ± 0.95	6.85 ± 0.8
Sun flower stem	1.70 ± 0.08	1.47 ± 0.09	0.0060 ± 0.0008	0.0085 ± 0.0009	6.41 ± 0.97	9.99 ± 1.00
Corn cob	0.34 ± 0.02	0.89 ± 0.01	0.0026 ± 0.0004	0.0065 ± 0.0006	8.78 ± 0.82	11.14 ± 1.32
Sawdust	0.60 ± 0.02	1.02 ± 0.08	0.0033 ± 0.0007	0.0062 ± 0.0008	4.48 ± 0.64	7.33 ± 0.89

490 **Table 2.** Crystallinity degree and crystallite size of untreated, delignified (TC) and hydro-
491 lyzed freeze dried cellulosic materials.

Cellulosics	Percentage of crystallinity (%)			Crystal size (nm)		
	Untreated	TC	Hydrolyzed	Untreated	TC	Hydrolyzed
Wheat straw	53.0	61.6	66.5	31.7	3.3	3.9
Sunflower stem	66.2	57.7	61.9	31.2	3.0	3.8
Corn cob	45.3	58.0	61.6	30.7	3.1	3.6
Sawdust	56.6	60.8	59.5	30.4	3.3	3.5

492

493 **Table 3.** Porosimetry analysis of freeze dried samples from supernatant during corn cob's hy-
494 drolysis with cellulase.

495

	BET Surface area (m²/g)	Pore volume_(BJH) (cm³/g)	Pore size_(BET) (nm)
24 h	0.79±0.03	0.0040±0.0001	3.60 ± 0.2
72 h	1.35±0.1	0.0069±0.0005	4.60 ± 0.6
168 h	0.20±0.009	0.0011±0.0003	1.65 ± 0.3
336 h	0.35±0.04	0.0025±0.0002	1.60 ± 0.3

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497 **Table 4.** Investment cost. Equipment cost for plant installation.

Machinery	Capacity	Price (€)
Delignification tank	100,000 L	30,000
Enzyme production bioreactor	10,000 L	20,000
Sterile filter	150 m ³ /min	9,000
Air pump	150 m ³ /min	20,000
CHNTs production bioreactor	100,000 L	30,000
Pump	4 m ³ /h	2,000
Centrifugal separator	20 m ³ /h	150,000
Tank for CHNTs solution	100,000 L	30,000
Condenser	3.3 m ³ /h	300,000
Freeze dryer	6000 Kg water/day	500,000
Boiler	2500 Kg oil/day	600,000
Pump	20 m ³ /h	2,000
Vacuum pump	5 HP	20,000
Pipe lines		30,000
Total		1,743,000

498 **Table 5.** Daily Production Cost. Parameters affecting the production cost.

499

Parameter	Cost (€/day)
Raw material	400
Labor cost	1,070
Thermal energy	830
Electricity	35
Water requirement	40
Consumables	205
Investment payments	156
Total	2731

1 **Carbohydrate Nano-tubes Production and its Techno-economic Validation**

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12 **ABSTRACT**

13 ~~The p~~roduction of carbohydrate-nano-tubes (CHNTs) using agricultural wastes is proposed
14 in this investigation. The corncob was found to be the most productive for our purpose among
15 the four lignocellulosic raw materials tested. CHNTs production was accomplished in two
16 stages. Tubular ~~Cellulose-cellulose~~ (TC) was prepared from raw substrates through a deligni-
17 fication process, and the prepared tubes of TC were cut ~~to~~into nano-size carbohydrate-tubes
18 in a chemical-free process. To achieve this, cellulase was produced in our lab using agricul-
19 tural residue, employing ~~a high cellulase producer~~ the non-pathogenic ~~fungi~~ fungus *Tricho-*
20 *derma reesei*, ~~a high cellulase producer~~. Analysis of ~~the~~ produced CHNTs proved stability,
21 nano-dimension lengths, and increased crystallinity. The technoeconomic feasibility report
22 showed that the production of CHNTs is cost-effective. This was supported by a process flow
23 sheet with mass and energy balances based on laboratory experimental results.

24 **KEYWORDS:** *corncob; cellulose; Trichoderma reesei; cellulase; hydrolysis; Carbohydrate*
25 *nano-tubes.*

26

27

28 1. Introduction

29 Over the past few decades, nanotechnology, nano-synthetic materials, and their applications have
30 gained attention. Carbon ~~Nano Tubes~~ nanotubes (CNTs) are among the most commonly used nano-
31 materials. These CNTs are rolled graphene with sp^2 hybridization and can be divided into three cate-
32 gories, according to the number of tubes present in CNTs: single-walled CNTs, double-walled CNTs, and
33 multi-walled CNTs (Eatemadi et al., 2014; Ibrahim, 2013). Information on CNTs was first published in
34 1991 (Lijima, 1991), and since then this nano-material has established rapidly growing applications in
35 sensors, nano-medicine, environment, energy, and others (Ibrahim, 2013). However, their use in the
36 biological and biomedical sectors ~~for of the~~ human system is restricted due to their increased toxicity
37 to the human body. The size of nanotubes can affect the toxicity of CNTs, particularly those with a size
38 under 100 nm. They can affect the lungs and whole respiratory system by activating immunological
39 responses, modifying protein structure, and these re-disperse from their site of deposition in the human
40 system (Eatemadi et al., 2014; Satishkumar et al., 2000). ~~The p~~ Prolonged and excessive exposure to
41 CNTs can cause inflammation and oxidative stress (Nemmar et al., 2001).

42 In order to avoid the side effects ~~of~~ of CNT use, we anticipated that alternative agricultural materials,
43 could be used for nanotubes production. Inexpensive and renewable natural resources were explored
44 for the production of carbohydrate nano-tubes (CHNTs). Such materials can be made from residual
45 plants stalks, which are generated as by-products of each crop. Globally, enormous amounts of agricul-
46 tural waste, such as wheat straw, sunflower stems, and corncobs, are produced each year following the
47 harvesting of wheat grains, corn, and sunflower seeds. (Barouni et al., 2015; Bian et al., 2018; Cavali
48 et al., 2020; Chen et al., 2021; FAO, 2019; Koutinas et al., 2016a; USDA, 2021). Nanofibers produced
49 from natural cellulosic waste materials and their application in nanocomposite materials ~~is a topic~~
50 ~~of~~ are topics in Green-Advance. The advantages of cellulose nanofibers include their biodegradability,
51 biocompatibility, renewable nature, high strength and stiffness, and low weight. (Kumar et al., 2020;
52 Reddy and Rhim, 2014; Sosiati et al., 2014). Furthermore, nanocellulose's structure can be modified to
53 meet the needs of particular applications by not only using a particular agricultural product as the ma-

54 terial's initial carbon source but also by improving or changing the method of production. Nanocellu-
55 loses have ~~proved~~ proven to be possible fillers for the improvement of the mechanical properties of
56 biopolymer films, such as starch, alginate, and chitosan films (Barouni et al., 2015; Koutinas et al.,
57 2016a; Kumar et al., 2020; Reddy and Rhim, 2014; Shankar and Rhim, 2016). Our previous studies
58 have shown that lignocellulosic material after delignification- can be used for the formation of tubular
59 cellulose-; with micro and nano dimensions (Koutinas et al., 2016b). The aim of this work was the pro-
60 duction of carbohydrate-nanotubes (CHNTs), a new generation of nano-tubes, from the carbon content
61 of agricultural residues via the preparation of tubular-cellulose (TC) in an enzymatic process.

62 2. Experimental

63 2.1 Agricultural residual materials

64 In our experiments, we used free or low-cost materials such as corncob and sunflower stems from lo-
65 cal farms, wheat straw from a local cattle feed market, and sawdust from a local timber mill.

66 2.2 Cellulase preparation

67 For a green- economical technology, we used cellulolytic enzymes- prepared in our lab from carbon
68 sources- of agricultural origin. A high cellulase-producer- *Trichoderma reesei* (ATCC 26921)-, was
69 grown on Potato Dextrose Agar (PDA) medium at 30 °C for 5-7 days. Fungal spores were aseptically
70 collected from the surface of PDA plates- by gently scraping with sterilized water and were counted
71 on a hemocytometer (Neubauer Improved, HBG, Germany). The production of cellulase was carried
72 out using a modified method ~~of~~ by Li et al. (2013). Two mL of spore suspension containing 10^6 - 10^7
73 spores mL^{-1} was precultured in 60 mL of sterilized medium consisting of 2%- w/v delignified sawdust,
74 1% soy peptone- and 1% glucose. The pH of the medium was adjusted ~~at~~ to 4.5 with a 2M NaOH solu-
75 tion and incubated in a VELP Scientifica FOC incubator at 30 °C and 180 rpm for 24 h. Forty mL of
76 freshly grown preculture was aseptically added into a 2 L bioreactor (Electrolab), containing 1 L of
77 sterilized medium made of 25 g delignified sawdust, 1.7% soy peptone, 0.5% $(\text{NH}_4)_2\text{SO}_4$, 0.6%
78 KH_2PO_4 , 0.2% $\text{MgSO}_4 \cdot 7\text{H}_2\text{O}$, 0.25% glycerol- and 2 mL Tween 20. The bioreactor equipped with the
79 control devices Fermac 231/260 was operated at 26 °C, 300 rpm, ~~ventilation~~ 1.5 L/min ventilation and

80 pH 4.5—5.0. After 150 h of fungal growth, the content was aseptically centrifuged to obtain a clear
81 supernatant for use as a crude preparation of cellulolytic enzyme.

82 2.3 Assay of cellulase activity

83 One mL of crude enzyme (prepared as above) was mixed with 100 mL of sodium citrate buffer (pH
84 5.0). From this, 5 mL was placed in a 50 mL conical flask with 10 mL of buffer and 0.5 g of finely
85 stripped Whatman filter paper. The reaction mixture was incubated at 50 °C for 60 min, and the re-
86 leased glucose due to enzyme activity was measured by High Performance Liquid Chromatography
87 (HPLC) on a Shimadzu LC-9A. Enzyme units were calculated against a standard curve plotted for glu-
88 cose released in a similar reaction conducted with a commercial cellulase with known units (Chu et al.,
89 2012).

90 2.4 Stage-1 Preparation of tubular cellulose (TC)

91 Lignocellulosic materials, including corncob, sunflower stem, wheat straw, and sawdust, were sub-
92 jected to a very mild (1%, w/v) NaOH solution treatment for three hours at 70 °C. Materials were fil-
93 tered out and washed with hot (90 °C-95 °C) deionized water for complete removal of NaOH and re-
94 leased lignin. The delignified material produced in this procedure was employed as TC in a later stage;
95 therefore, it was freeze-dried at 15×10^{-3} mbar and -45 °C using a Labtech Daihan Freeze Dry System.

96 2.5 Stage-2 Enzymatic treatment of TC to develop CHNTs

97 ~~In separate flasks containing 200 mL of buffer pH 5.0 and 10 mL of crude enzyme, 15 g of TC pre-
98 pared from four agricultural residues were incubated at 50 °C for 72 hours without stirring or mixing.
99 Fifteen g each of TC prepared from four agricultural residues material were placed in separate flasks,
100 with 200 mL of buffer pH 5.0 and 10 mL of crude enzyme and incubated at 50 °C for 72 h, without
101 any stirring or mixing.~~ To examine the formation of CHNTs samples from the flasks of each substrate
102 were taken at 5, 24, 48, and 72 h intervals.

103 2.6 Stage-3 Isolation of CHNTs

104 After hydrolysis of TC ~~an amount a quantity~~ of clear supernatant liquid ~~and~~ without dispersed solids
105 was taken, in order to isolate ~~the CHNTs soluble in~~ the water-soluble CHNTs. The liquid was freeze-
106 dried, and porosimetry and TEM analysis were performed in the ~~received~~ powder ~~received~~.

107 2.7 Examination of CHNTs

108 Following all Standard Operating Procedures (SOPs) for each equipment used, examination of CHNTs
109 ~~were was~~ conducted as below: ~~specific~~ Specific surface area, pore size distribution, and pore volume
110 of all types of materials (original raw material, TC, ~~and~~ CHNT) was carried out by N₂ adsorption-de-
111 sorption process at -196.15 °C on a Tristar 3000 porosimeter (Micromeritics); Jeol Model JSM-
112 5600LV scanning electron microscope was used operating at an accelerating voltage of 20 kV; X-ray
113 powder diffractometry (XRD) was used to test the crystallinity of materials on a Bruker AXS D8
114 ADVANCE at 40 kV and 20 mA. Segal's equation based on the diffraction pattern intensity was used
115 for the calculation of the crystallinity index (CI). Transmission Electron Microscopy (TEM) images
116 were taken with the help of a Gatan, model 782 Erlangshen E5500W camera. FTIR spectra of samples
117 were obtained using a FTIR Perkin-Elmer spectrophotometer, 16 PC model, in the range of 4000–400
118 cm⁻¹.

119 2.8 Technoeconomic validation and Process Flow Sheet for industrial application

120 Details of the process flow sheet design ~~is are~~ presented in Figure 5, and the investment and daily pro-
121 duction costs are presented in Tables 4 and 5, respectively. The delignification of biomass takes place
122 in ~~the~~ tank 1, by supplying steam ~~by through~~ a boiler (11) and the delignified cellulosic material is trans-
123 ferred to enzyme production bioreactor (2) and CHNTs production bioreactor (5). The enzyme produc-
124 tion bioreactor (2) is supplied with air by an air pump (4) through a sterile filter (3). The temperature
125 in bioreactors 2 and 5 is kept constant at 26 °C and 50 °C respectively, by supplying steam from the
126 boiler (11). The hydrolysate from the bioreactor 5 containing CHNTs is pumped to ~~the~~ centrifugal sep-
127 arator (7) to separate suspended solids from the solution of CHNTs. A clear CHNTs solution is col-
128 lected in tank 8, then concentrated in a condenser (9), and subsequently ~~is~~ freeze-dried in a freeze-
129 dryer system (10).

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131 3. Results and Discussion

132 3.1 Structure of TC

133 From the SEM images (Fig. S1) of wheat straw, sunflower stem, corncob, and sawdust (original and
134 delignified), it can be observed that the morphology of [the](#) materials ~~was~~ changed after delignification,
135 pores were created on the surface of the materials, and the fibers arranged in TC could be seen ([Fig.](#)
136 [S1.ref.supplementary.materials](#)). These changes are attributed to the removal of amorphous areas,
137 which was earlier occupied by lignin and hemicellulose contents in raw substrates (Cavali et al.,
138 2020). The two naturally occurring forms of cellulose are I α and I β . In this analysis, only I β was visi-
139 ble, as it is part of higher plants, in contrast to [the](#) form I α only found in bacterial and algae celluloses
140 (Poletto et al., 2014). Studies of atomic resolution synchrotron and neutron diffraction data, have
141 shown that cellulose I α has a triclinic unit cell P1 ($a = 6.717 \text{ \AA}$, $b = 5.9962 \text{ \AA}$,
142 $c = 10.400 \text{ \AA}$, $\alpha = 118.08^\circ$, $\beta = 114.80^\circ$, and $\gamma = 80.37^\circ$) containing a single cellulose chain, while ~~that~~
143 cellulose I β has a monoclinic unit cell P21 ($a = 7.784 \text{ \AA}$, $b = 8.201 \text{ \AA}$, $c = 10.380 \text{ \AA}$, $\alpha = \beta = 90^\circ$,
144 $\gamma = 96.5^\circ$) containing two conformationally distinct cellulose chains, called original chains and central
145 chain (Krichen et al., 2022). The structure of cellulose I β is mainly in [the](#) form of parallel chains
146 linked by H-bonds stacked with an alternating shear parallel to the chain axis stabilized by Van der
147 Waals interactions (Poletto et al., 2014). After delignification of materials, the specific surface area of
148 TC (Table 1) was about 2-fold higher due to the formation of cellulose tubes in the space created by
149 [the](#) removal of lignin fraction. The pore volume and pore size were also increased, except [for](#) TC pre-
150 pared from sunflower stem, which had [a](#) lower specific surface area (Table 1).

151 3.2 Crystallinity analysis

152 The degree of cellulose crystallinity plays an important role in cellulose structure parameters. Since
153 the crystal structure of cellulose affects the enzymatic ~~hydrolysis~~ (Park et al., 2010), the crystallinity
154 was examined in XRD analysis (Fig. 1 and Table 2). The characteristic peaks of I β cellulose were ob-
155 served at 2θ (theta) of about 16° , and 22.64° (Banvillet et al., 2021; Bian et al., 2018; Ling et al., 2021;

156 Zhang et al., 2021). The sharper peaks in the XRD profile of TC materials indicate that ~~its~~^{the} degree
157 of crystallinity was higher compared to that of the raw materials. For delignified sawdust, sunflower
158 stem₂ and wheat₂-straw, a peak located at 2θ of about 30.0° was also identified. This can be an indica-
159 tion of amorphous areas after delignification (Sosiati et al., 2015; Sosiati and Harsojo, 2014). Another
160 characteristic peak of cellulose I β at 2θ of about 35.0° appeared for all materials (Banvillet et al.,
161 2021; Ling et al., 2021; Zhang et al., 2021). An increase in the rigidity of cellulose tubes (fibers) and ^a
162 decrease in their flexibility occurs when there is an increase in the ratio of crystalline ~~to~~^{to} amorphous
163 regions. Sunflower stem and corn cob had the lowest crystallinity indices (CI) (Table 2). CI increases
164 as the surface area of the crystallites corresponds to decrease in amorphous cellulose, due to ^{the} void
165 spaces available after lignin removal (Cavali et al., 2020; Poletto et al., 2014).

166 3.3 FT-IR spectra

167 The spectra for corncob and wheat-straw are presented in Figs. 2a and 2b, for the other two materials,
168 spectra were similar (hence not presented here). At around $3440\text{-}3420\text{ cm}^{-1}$ an intramolecular H-bond
169 vibration appeared, which indicates cellulose (Poletto et al., 2014). The FTIR absorption peaks at
170 $\sim 2900\text{ cm}^{-1}$ are characteristic of the stretching vibration of C-H groups of cellulose (Reddy and Rhim,
171 2014). The absorption peaks at $1440\text{-}1430\text{ cm}^{-1}$ are due to CH_2 bending vibration and indicates^s the
172 “crystallinity band” in the cellulose. A reduction ~~or~~^{or} expansion in the intensity of this crystallinity band
173 among the untreated, delignified freeze dried₂ and after enzymatic hydrolysis samples indicates that
174 the level of crystallinity of cellulose crystals decreased/increased during treatment₂-processes (Shankar
175 and Rhim, 2016). The peaks appeared at 1375 cm^{-1} are typical of the O-H bending vibration of cellu-
176 lose. The peaks at $1163\text{-}1165\text{ cm}^{-1}$ are attributed to the C-O-C pyranose ring stretching vibration and
177 the peaks at $896\text{-}898\text{ cm}^{-1}$ indicate ^{the} C-H rocking vibration of cellulose present in the microfibers
178 and nanofibers (Reddy and Rhim, 2014). No considerable changes in ^{the} absorption peaks positions of
179 untreated and delignified freeze₂-dried samples (TC), were observed (Figs. 2a and 2b), which indicated
180 that these processes did not alter the chemical structure of the cellulosic materials. However, the spec-
181 tra bands present at around 1730 cm^{-1} in raw lignocellulosic (due to C-O stretching vibration for the
182 acetyl and ester linkages in lignin/hemicellulose) were absent in ^{the} spectra of TC. That confirmed the

183 absence of lignin and hemicellulose in TC, which were removed in stage_1 of alkali treatment (Ga-
184 briel et al., 2020; Kargarzadeh et al., 2012; Kumar et al., 2020).

185 3.4 Enzyme_treatment of TC for development of CHNTs

186 TC materials were treated with our lab-prepared crude cellulase (70 FPU/g) to develop CHNTs. N₂ ad-
187 sorption-desorption porosimetry analysis (Figs. 3a, b, c) show the kinetics: BET surface area (m²/g) and
188 pore volume are given by BJH equation, and the pore size by BET (nm). CHNTs were produced after
189 24 h enzyme treatment of TC obtained from four agricultural_substrates. CHNTs from corn cob pre-
190 sented the highest value of surface area (1.8 m²/g), which is a desired parameter for the entrapment of
191 pharmaceutical substances, food preservatives, and other entities in CHNTs (Panitsa et al., 2021).
192 Based on the number of tubes with pore widths between 2-70 nm (Fig. 3d) in combination with pore-
193 volume (0.013 cm³/g) and the average pore diameter (13.5 nm), corncob-TC proved to be the most
194 productive material among the TC of other substrates, for the development of CHNTs.

196 3.5 Physicochemical properties of the isolated CHNTs product

197 CHNTs retain some important properties of cellulose, such as biodegradability and non-tox-
198 icity. CHNTs are oligomers having-with glucose as their structural unit, and can form hydro-
199 gen bonds with OH groups containing enzymes and drugs. The characterization of the isolated
200 product of CHNTs was carried out by TEM to prove the nano-dimensions of the length of
201 tubes. Porosimetry analysis confirmed the pore size (Table 3) and pore distribution (Fig. S3),
202 classifying the material as a nanomaterials.

203 3.5.1 Transmission Electron Microscopy of the isolated CHNTs product

204 TEM images of CHNTs developed from corncob showed needle-like cellulosic nanotubes
205 (Fig. 4 a,b) with an internal diameter 6-16 nm and a length of tubes in the range of 80-160

206 nm. These data proved that the cellulosic tubes in TC after ~~the~~ treatment with cellulolytic en-
207 zymes produced carbohydrate nanotubes ~~CarboHydrate Nano Tubes~~ (CHNTs).

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208 3.5.2 Porosimetry analysis of the isolated CHNTs product

209 The BET surface area was 1.35 m²/g and the pore width was 4.6 nm after 72 hours of hydrol-
210 ysis, as shown in Table 3 (supplementary materials). Porosimetry measurement revealed an
211 average pore diameter (tube diameter) of around 4-5 nm (Fig. 4b), which is consistent with
212 the size of the tubes depicted in the TEM image. Table 3 shows that after 72 h of hydrolysis,
213 the pore width was 4.6 nm with a volume of 0.0069 cm³/g and a BET surface area of 1.35
214 m²/g (ref supplementary materials). The average pore diameter (tube diameter) of about 4-5
215 nm measured with porosimetry analysis is comparable with the size of tubes shown in the
216 TEM image (Fig. 4b).

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217 3.6 Design and operation of the bioreactor and economic validation of technology

218 The bioreactor system presented in Figure 5 contains ~~the~~ bioreactor 2 of 10,000 L for enzyme produc-
219 tion and ~~the~~ bioreactor 5 of 100,000 L for tubular cellulose (TC) hydrolysis to nano-tubes. Machineries
220 of high cost are the condenser (9), freeze dryer (10) and centrifugal separator (7). The boiler (11) of
221 ~~850 litres~~ liters of oil per day and the delignification tank (1) are also of importance. Delignification
222 tanks (1) and condensers (9) need about 87% of steam consumption. Centrifugal separator (7) and
223 freeze dryers (10) need more ~~of than~~ 90% electricity consumption. The total investment cost has been
224 calculated ~~to at~~ €1,743,000 ~~with~~ 1,743,000 with the bigger cost to be that of condenser (€300,000),
225 freeze dryer (€500,000) and boiler ~~of~~ (€600,000). The parameters considered for the calculation of the
226 daily production cost were raw material cost, labor, thermal energy, electricity, water requirement,
227 consumables, and investment payment costs. The biggest costs are the labor cost and that of thermal
228 energy, which are about 70% of the €2,731 -daily cost. ~~On the other hand, the annual turnover is equal~~

229 to about €1,500,000, which could give a profit of €300,000 annually. So, it is estimated that the pay-
230 ment of investment costs will be achieved in about 6 years. This short period of investment repayment
231 shows that the technology has a large margin of profit to convince the investors to proceed.

232 3.7. Technological and scientific implications

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233 The aforementioned presentation of results and discussion have demonstrated the production
234 of CHNTs. Specifically, the XRD and FTIR analysis proved that the tubes consist of cellulose,
235 while lignin and hemicelluloses have been removed. They also proved the increment of crys-
236 tallinity indices, which is related with-to the rigidity of tubes. The formation of a new genera-
237 tion of tubes, could lead to the preparation of a carrier material potentially usable as a drug
238 delivery system. The metabolism and safety of CHNTs in the human body should be exam-
239 ined. Immobilization of cellulase in CHNT tubes with pharmaceutical substances could be
240 considered as a possible method for removing the carrier material from the body, after its ac-
241 tion. Cellulase, has the ability to hydrolyze cellulose into glucose, a nutrient for humans. Fi-
242 nally, the method of producing CHNTs is feasible, and the raw material is sustainable. The
243 technoeconomic validation based on laboratory results showed that the process is cost-effective.
244 This is supported by laboratory results (ref see supplementary material Table S1).

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246 4. Conclusions

247 The Technoeconomic feasibility report validated that CHNTs production is cost-effective. A Green
248 green technology was used, using was applied for four agricultural residual materials. Among them,
249 corncob has proved the most productive. It is free of cost, making our process economically viable.
250 TC tubes from corncob were cut short with cellulase, a cheaper lab preparation from *Trichoderma*
251 *reesei*, to carbohydrate tubes of nano-size. FTIR and XRD analysis revealed the stability of CHNT's
252 chemical structure. CHNTs were isolated from the solution of hydrolysed/hydrolyzed cellulose after

253 freeze-drying. The nano-dimension tubes of the final product were confirmed by TEM and ~~with~~ po-
254 rosimetry analysis. CHNTs-~~based -a~~ carrier materials could potentially be used as drug delivery sys-
255 tems. However, their metabolism in ~~the~~ human body should be studied for their safety.

256

257 E-supplementary data for this work can be found in e-version of this paper online

258 .

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273 The authors declare that they have no known competing financial interests or personal [relation](#)
274 [ships](#) [relationships](#) that could have appeared to influence the work reported in this paper.

275 **CRedit authorship contribution statement**

276 All authors contributed to the study conception and design. **Athanasia Panitsa**: Methodol-
277 ogy, Validation, Investigation, original draft, Visualization. **Theano Petsi**: Methodology,
278 Writing-review & editing. **Eleana Kordouli**: Methodology, Validation. **Poonam S. Nigam**:
279 Result-analysis for writing-second draft, editing. **Maria Kanellaki**: Supervision. **Athanasios**
280 **A. Koutinas**: Conceptualization, Writing-original draft, Project-administration, Funding-ac-
281 quisition. All authors read and approved the final manuscript.

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378

379 **Figure captions**

380 **Figure 1.** XRD spectra of (a) untreated and (b) delignified freeze dried cellulosic materials.

381 **Figure 2.** FTIR spectra of untreated (black), delignified freeze dried (blue) and after hydroly-
382 sis (red) (a) corn cob and (b) sawdust, (c) FTIR spectra of solid formed by freeze dried sam-
383 ples of the supernatant after: 24 h (black), 72 h (blue), 168 h (red) and 336 h (pink) of corn
384 cob's hydrolysis.

385 **Figure 3.** Porosimetry analysis of delignified cellulosic materials during their hydrolysis with
386 cellulase. (a) BET surface area (m^2/g), (b) Pore volume (BJH) (cm^3/g), (c) Pore size (BET)
387 (nm), (d) % pore volume between 2-70 nm of delignified freeze dried cellulosic materials dur-
388 ing their hydrolysis with cellulase enzymes.

389 **Figure 4.** (a) TEM image of hydrolyzed corn cob (solid part) after 24 h of hydrolysis, (b)
390 TEM image of solid formed by freeze-dried samples from supernatant after 72 h of corn cob's
391 hydrolysis.

392 **Figure 5.** Process flow sheet with mass (kg) and energy (kg of steam) balance for CHNTs
393 production. 1. Delignification tank (100 m^3); 2. Enzyme production bioreactor (10 m^3); 3.
394 Sterile filter ($150 \text{ m}^3/\text{min}$); 4. Air pump ($150 \text{ m}^3/\text{min}$); 5. CHNTs production bioreactor (100
395 m^3/min); 6. Pump ($4 \text{ m}^3/\text{h}$); 7. Centrifugal separator ($20 \text{ m}^3/\text{h}$); 8. Tank for CHNTs solution
396 (100 m^3); 9. Condenser ($3.3 \text{ m}^3/\text{h}$); 10. Freeze dryer – water removal (6000 kg/d); 11. Boiler
397 (2500 kg oil/day); 12. Pump ($20 \text{ m}^3/\text{h}$); 13. Vacuum pump 5Hp

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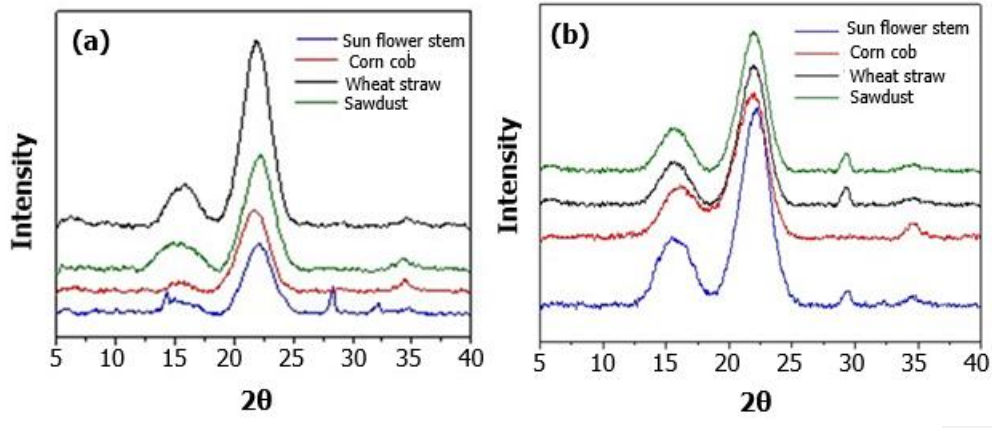


Figure 1.

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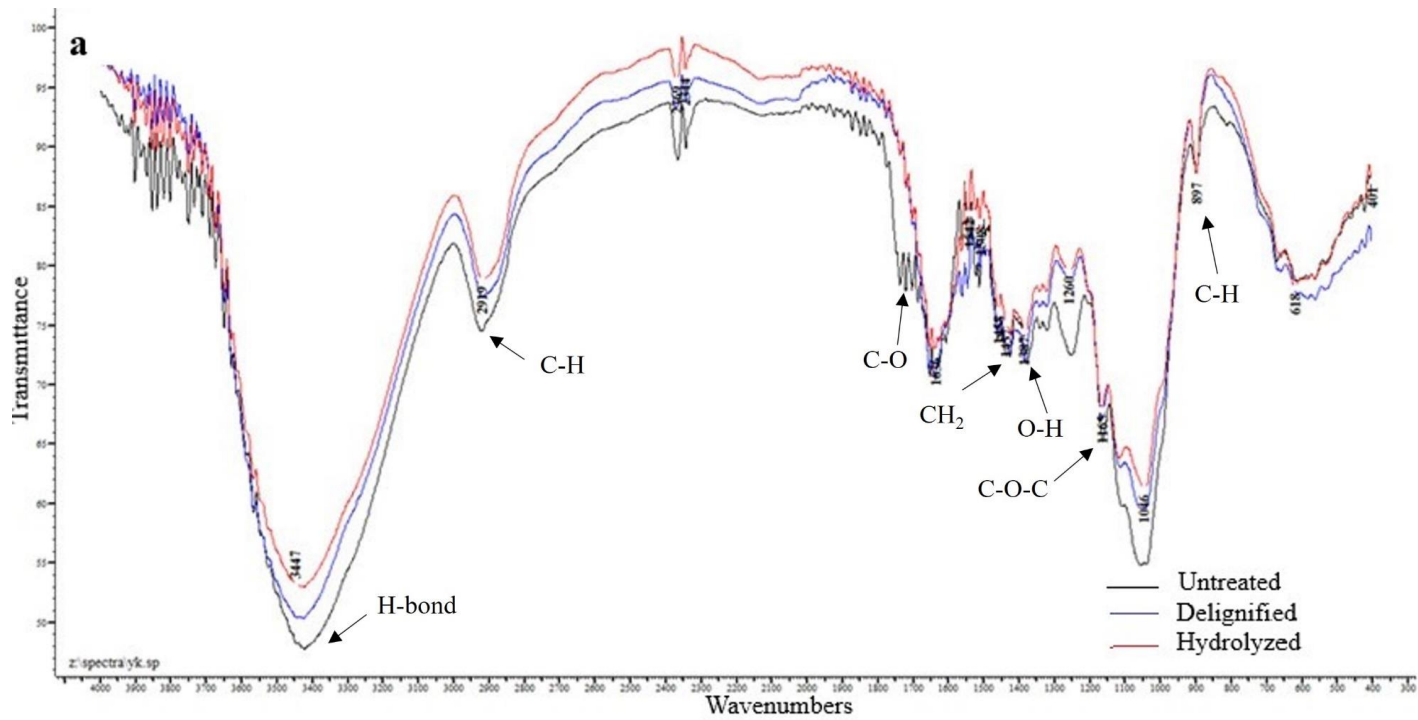
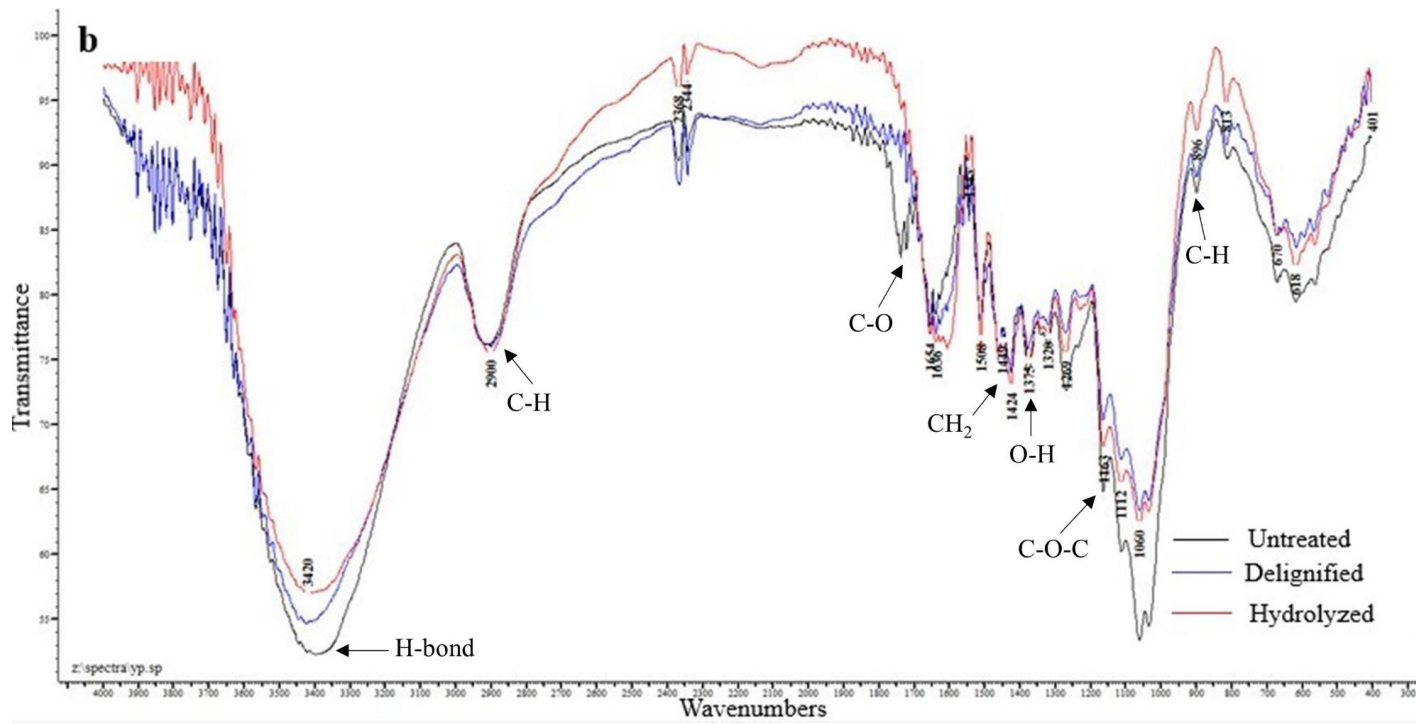


Figure 2a.

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Figure 2b.

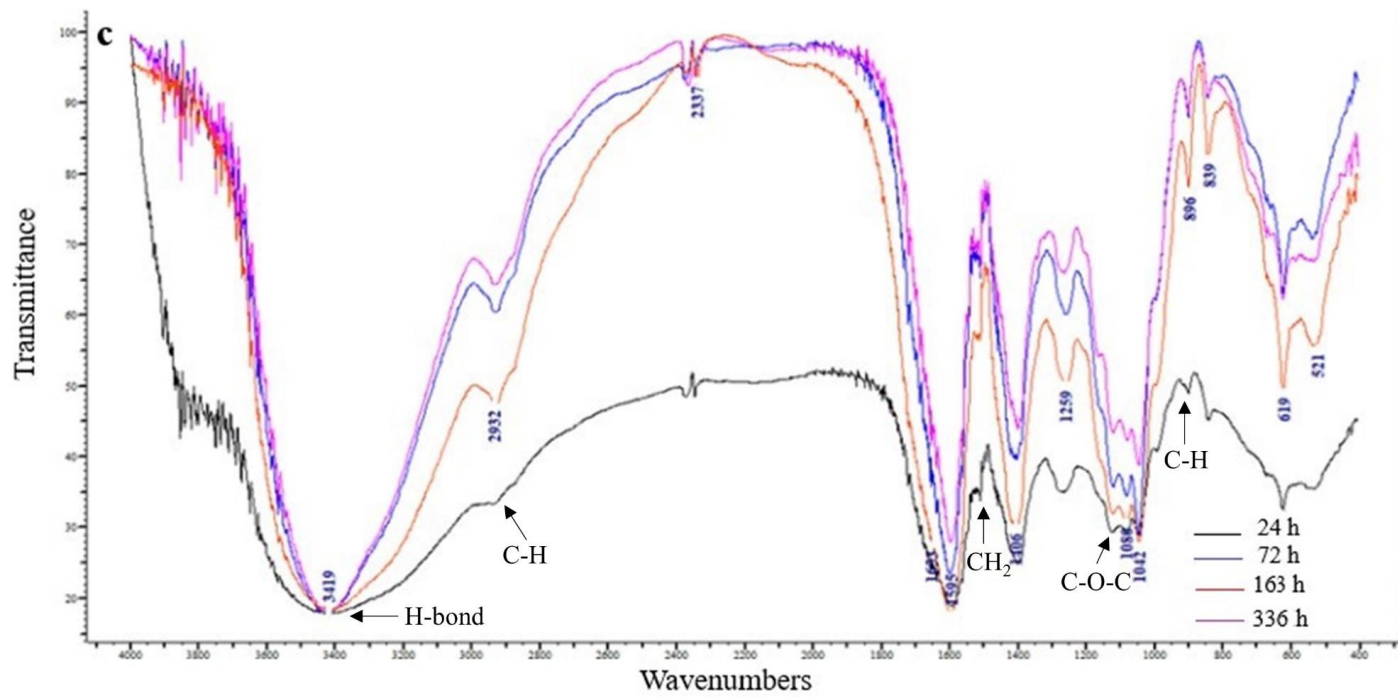


Figure 2c.

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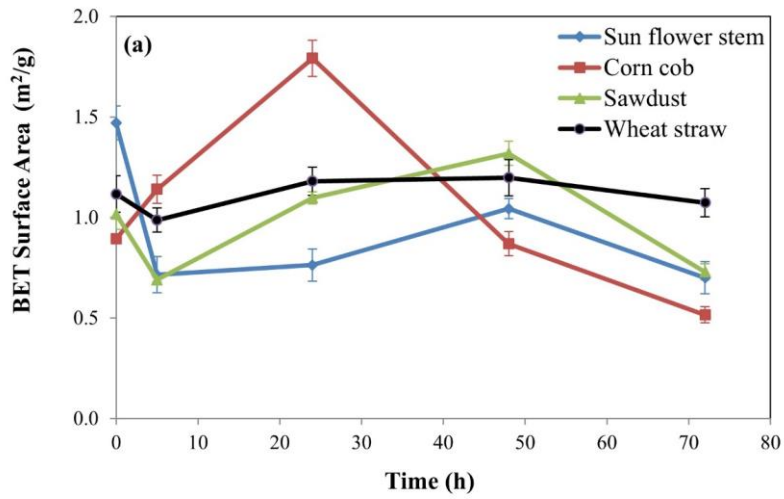


Figure 3a.

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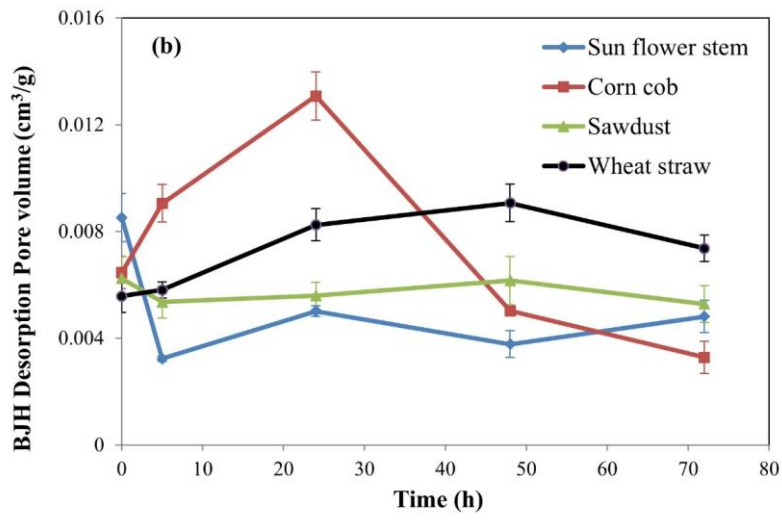


Figure 3b.

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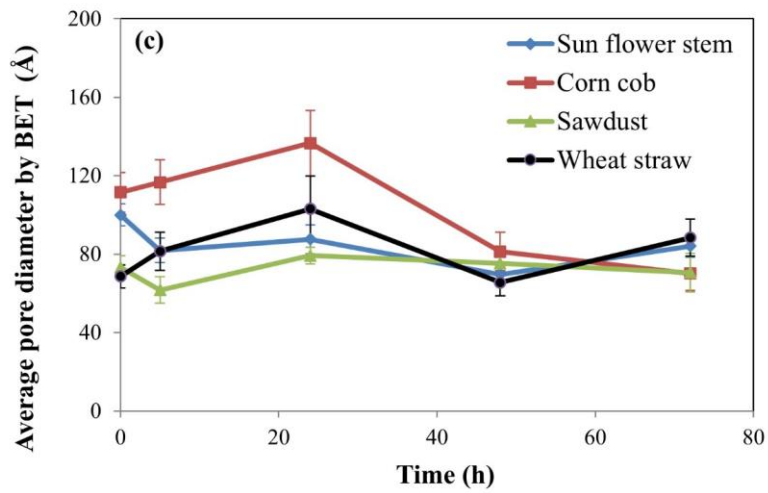


Figure 3c.

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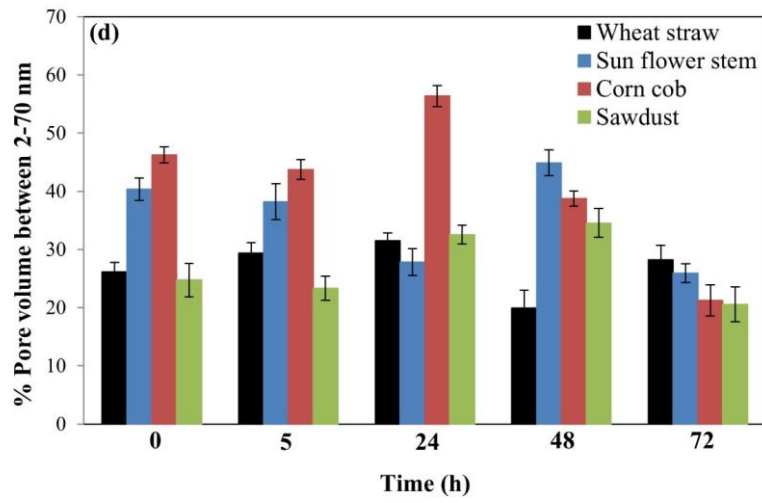


Figure 3d.

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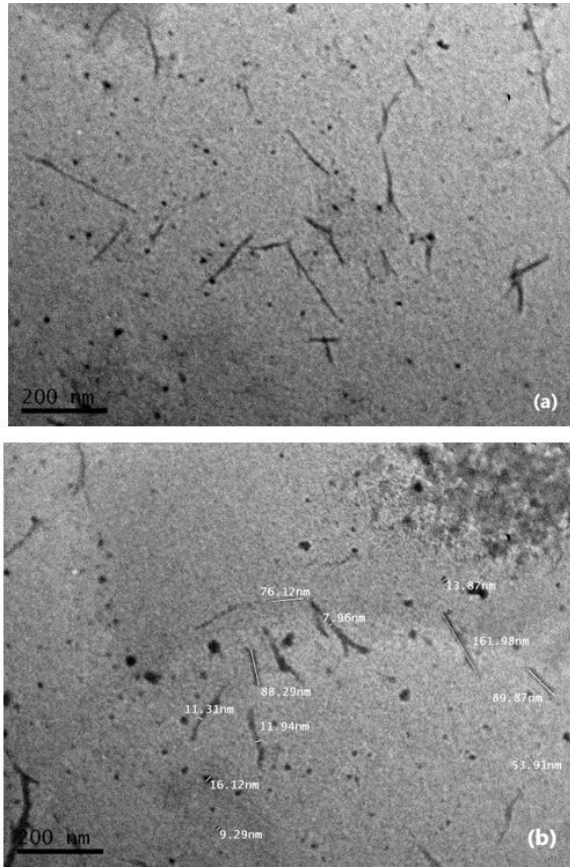


Figure 4.

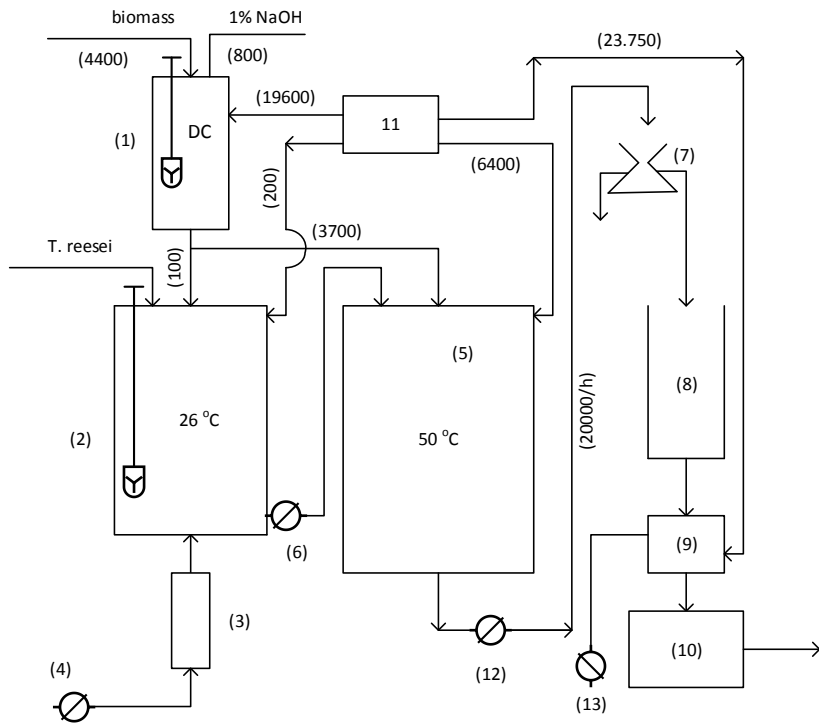


Figure 5.

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493 **Table 1.** Porosimetry analysis of untreated and delignified freeze dried (TC) cellulosic materi-
 494 als.
 495

Cellulosics	BET Surface area (m ² /g)		Pore volume _(BJH) (cm ³ /g)		Pore size _(BET) (nm)	
	Untreated	TC	Untreated	TC	Untreated	TC
Wheat straw	0.48 ± 0.01	1.12 ± 0.09	0.0034 ± 0.0006	0.0056 ± 0.0006	8.23 ± 0.95	6.85 ± 0.8
Sun flower stem	1.70 ± 0.08	1.47 ± 0.09	0.0060 ± 0.0008	0.0085 ± 0.0009	6.41 ± 0.97	9.99 ± 1.00
Corn cob	0.34 ± 0.02	0.89 ± 0.01	0.0026 ± 0.0004	0.0065 ± 0.0006	8.78 ± 0.82	11.14 ± 1.32
Sawdust	0.60 ± 0.02	1.02 ± 0.08	0.0033 ± 0.0007	0.0062 ± 0.0008	4.48 ± 0.64	7.33 ± 0.89

496 **Table 2.** Crystallinity degree and crystallite size of untreated, delignified (TC) and hydro-
 497 lyzed freeze dried cellulosic materials.

Cellulosics	Percentage of crystallinity (%)			Crystal size (nm)		
	Untreated	TC	Hydrolyzed	Untreated	TC	Hydrolyzed
Wheat straw	53.0	61.6	66.5	31.7	3.3	3.9
Sunflower stem	66.2	57.7	61.9	31.2	3.0	3.8
Corn cob	45.3	58.0	61.6	30.7	3.1	3.6
Sawdust	56.6	60.8	59.5	30.4	3.3	3.5

498

499 **Table 3.** Porosimetry analysis of freeze dried samples from supernatant during corn cob's hy-
500 drolysis with cellulase.

501

	BET Surface area (m²/g)	Pore volume_(BJH) (cm³/g)	Pore size_(BET) (nm)
24 h	0.79±0.03	0.0040±0.0001	3.60 ± 0.2
72 h	1.35±0.1	0.0069±0.0005	4.60 ± 0.6
168 h	0.20±0.009	0.0011±0.0003	1.65 ± 0.3
336 h	0.35±0.04	0.0025±0.0002	1.60 ± 0.3

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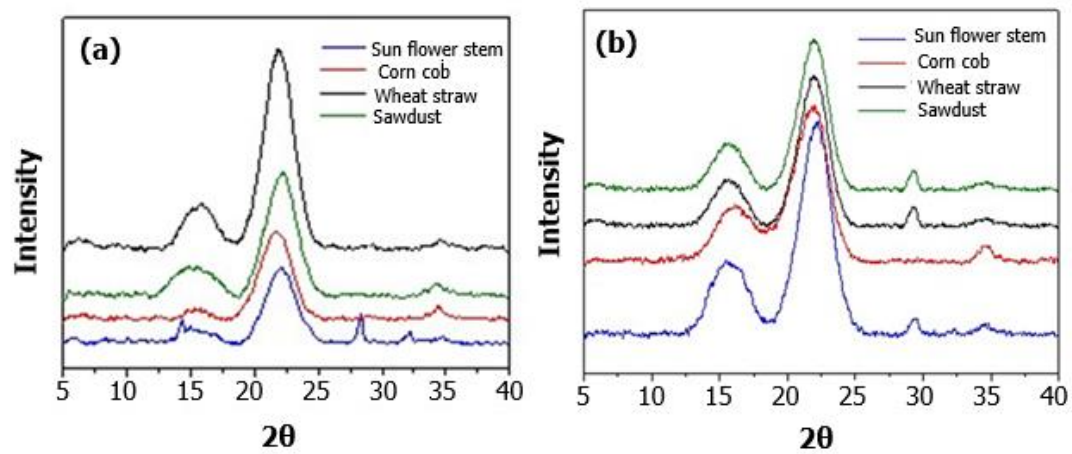
503 **Table 4.** Investment cost. Equipment cost for plant installation.

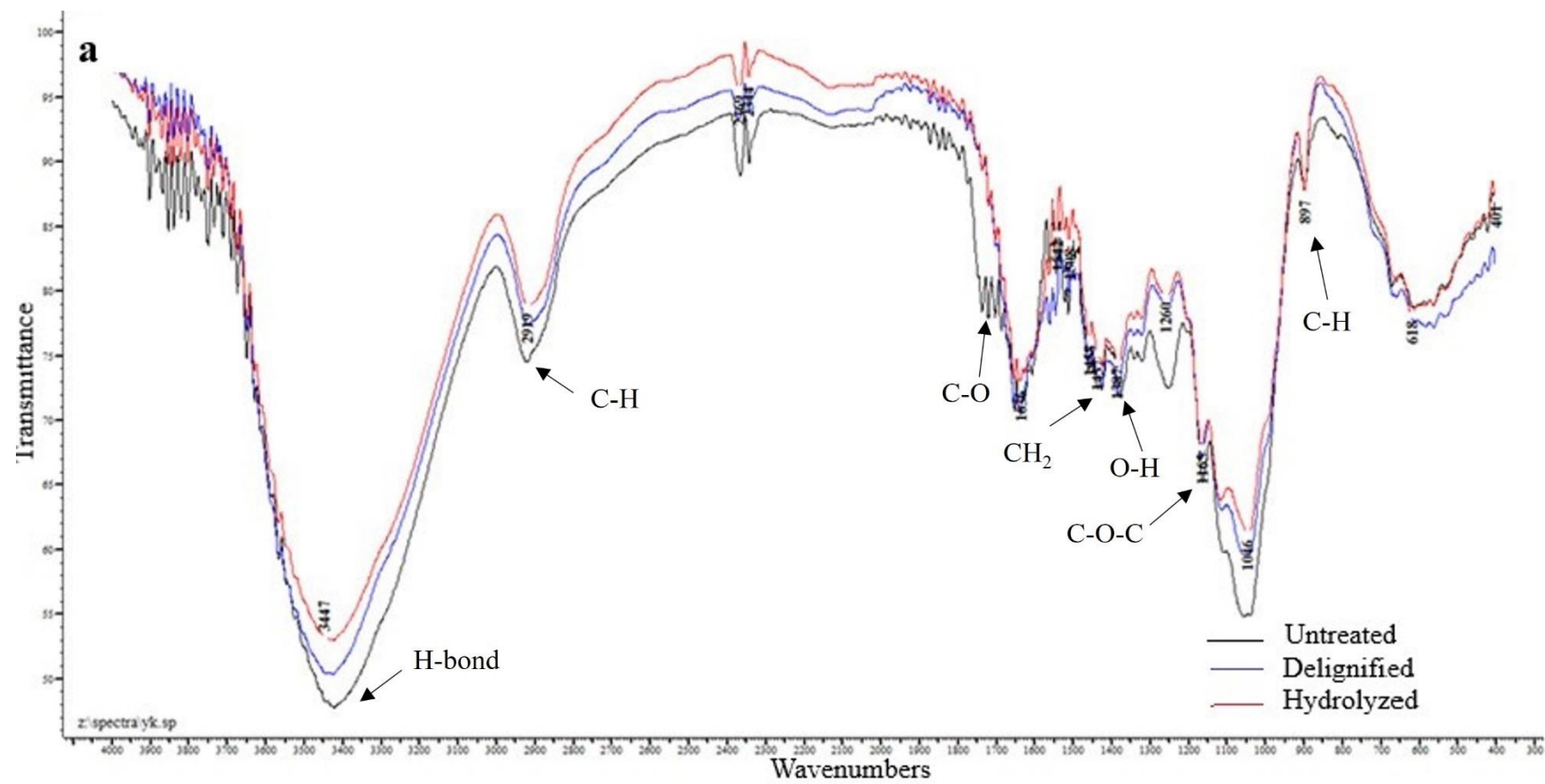
Machinery	Capacity	Price (€)
Delignification tank	100,000 L	30,000
Enzyme production bioreactor	10,000 L	20,000
Sterile filter	150 m ³ /min	9,000
Air pump	150 m ³ /min	20,000
CHNTs production bioreactor	100,000 L	30,000
Pump	4 m ³ /h	2,000
Centrifugal separator	20 m ³ /h	150,000
Tank for CHNTs solution	100,000 L	30,000
Condenser	3.3 m ³ /h	300,000
Freeze dryer	6000 Kg water/day	500,000
Boiler	2500 Kg oil/day	600,000
Pump	20 m ³ /h	2,000
Vacuum pump	5 HP	20,000
Pipe lines		30,000
Total		1,743,000

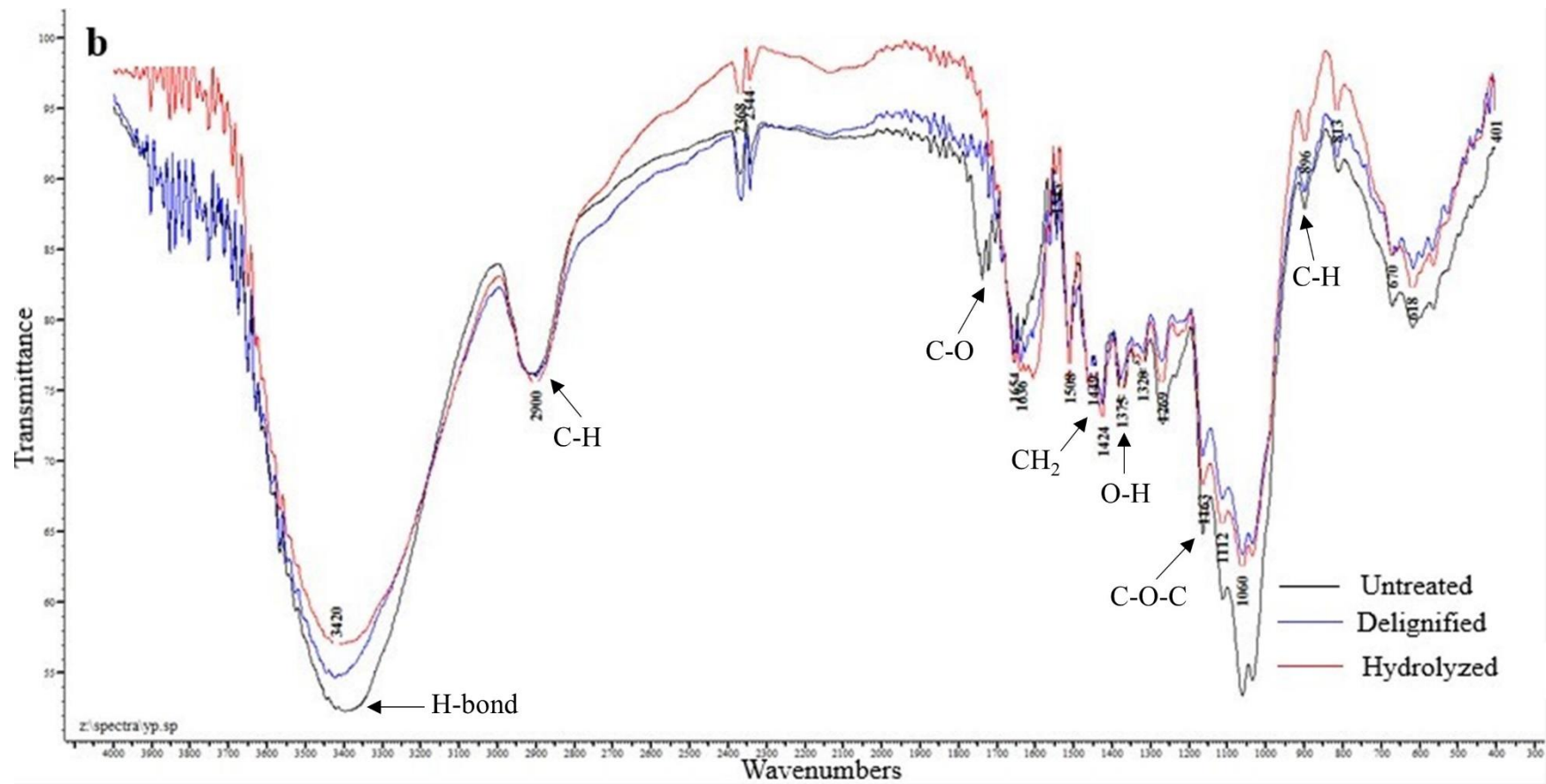
504 **Table 5.** Daily Production Cost. Parameters affecting the production cost.

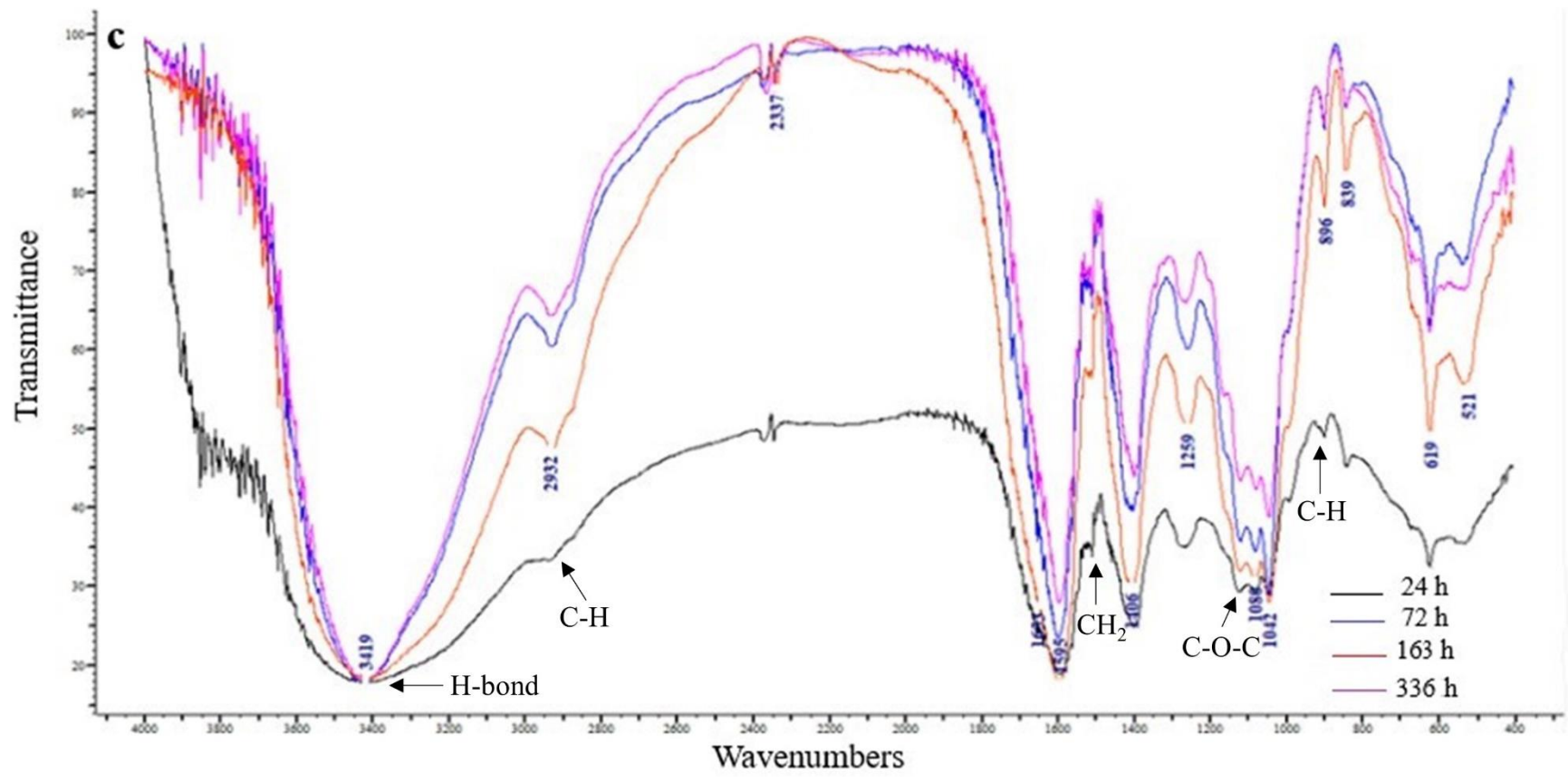
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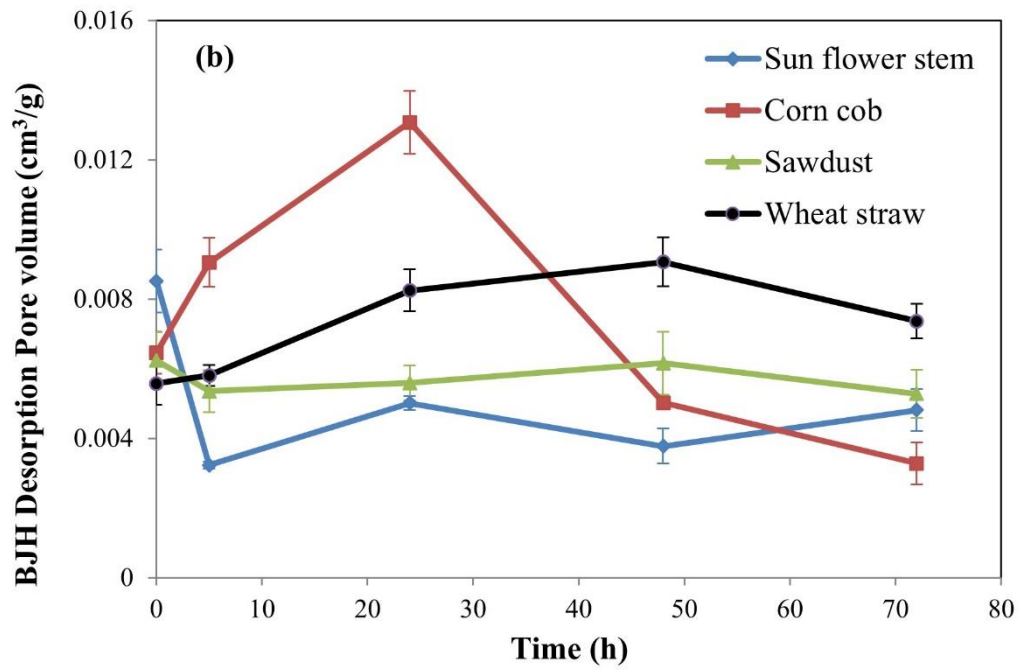
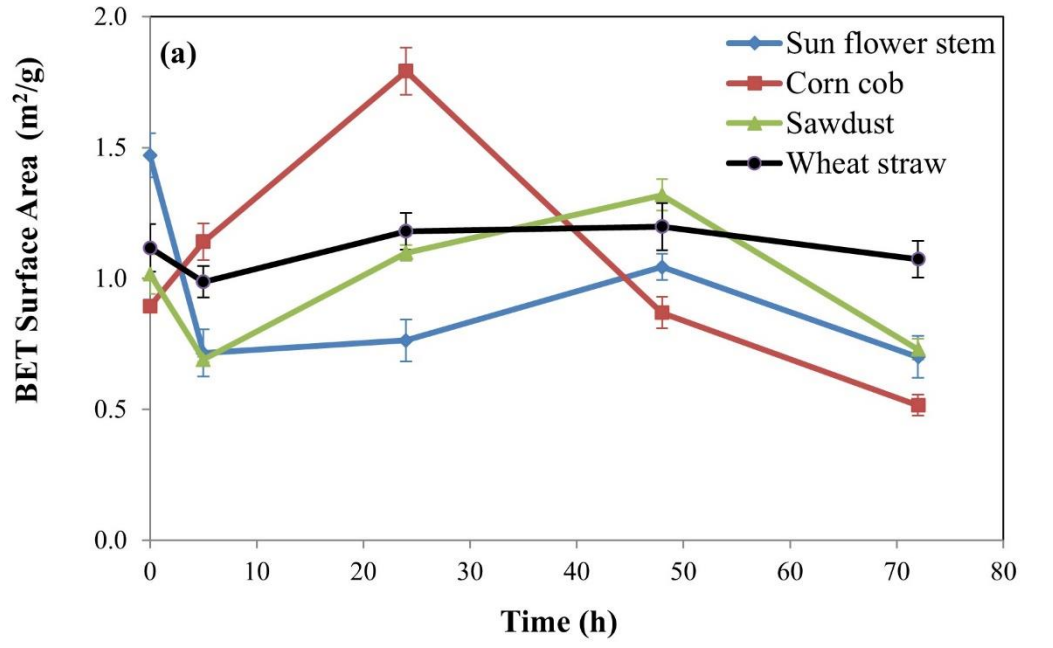
Parameter	Cost (€/day)
Raw material	400
Labor cost	1,070
Thermal energy	830
Electricity	35
Water requirement	40
Consumables	205
Investment payments	156
Total	2731

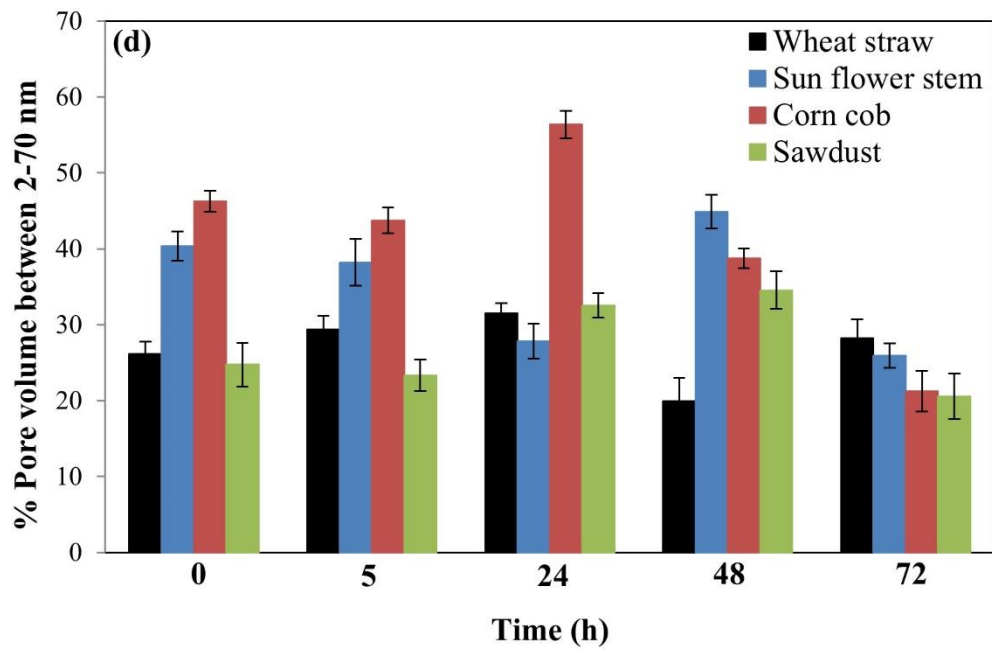
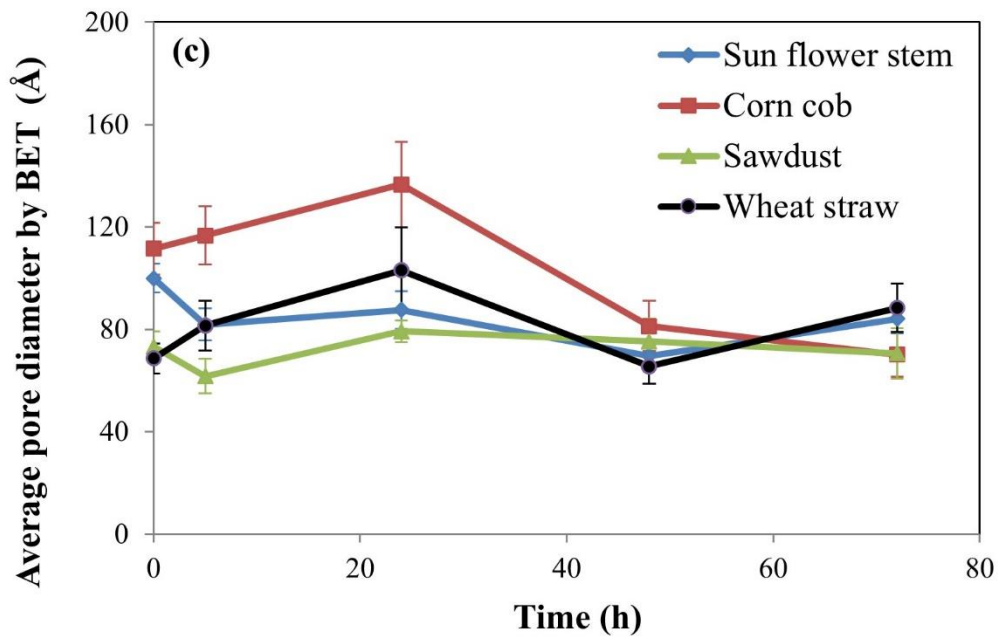


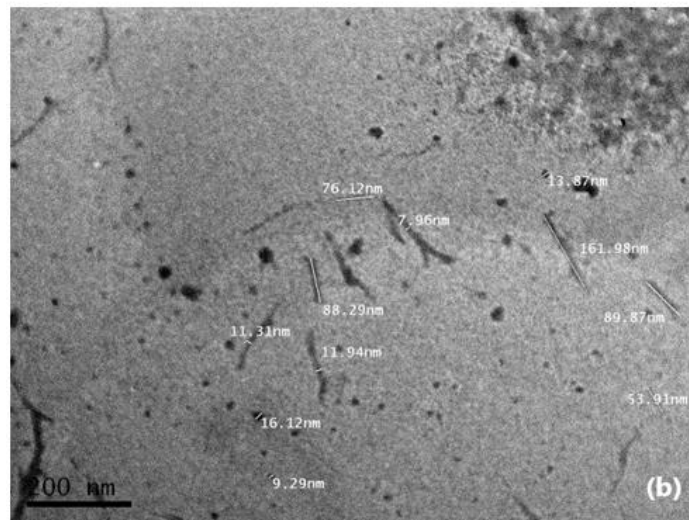
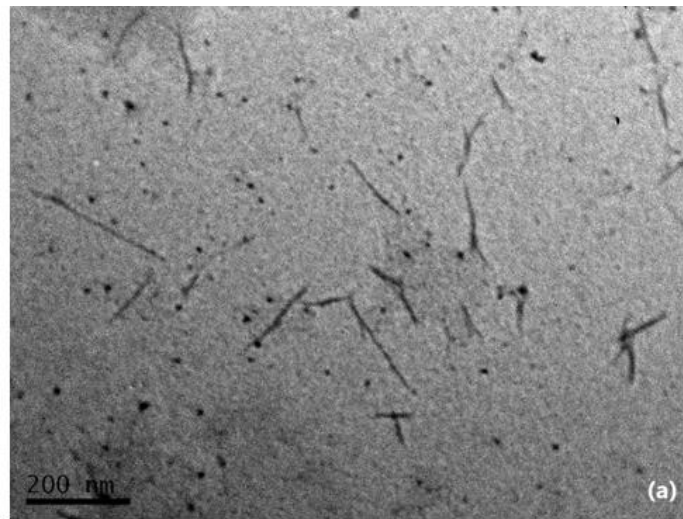


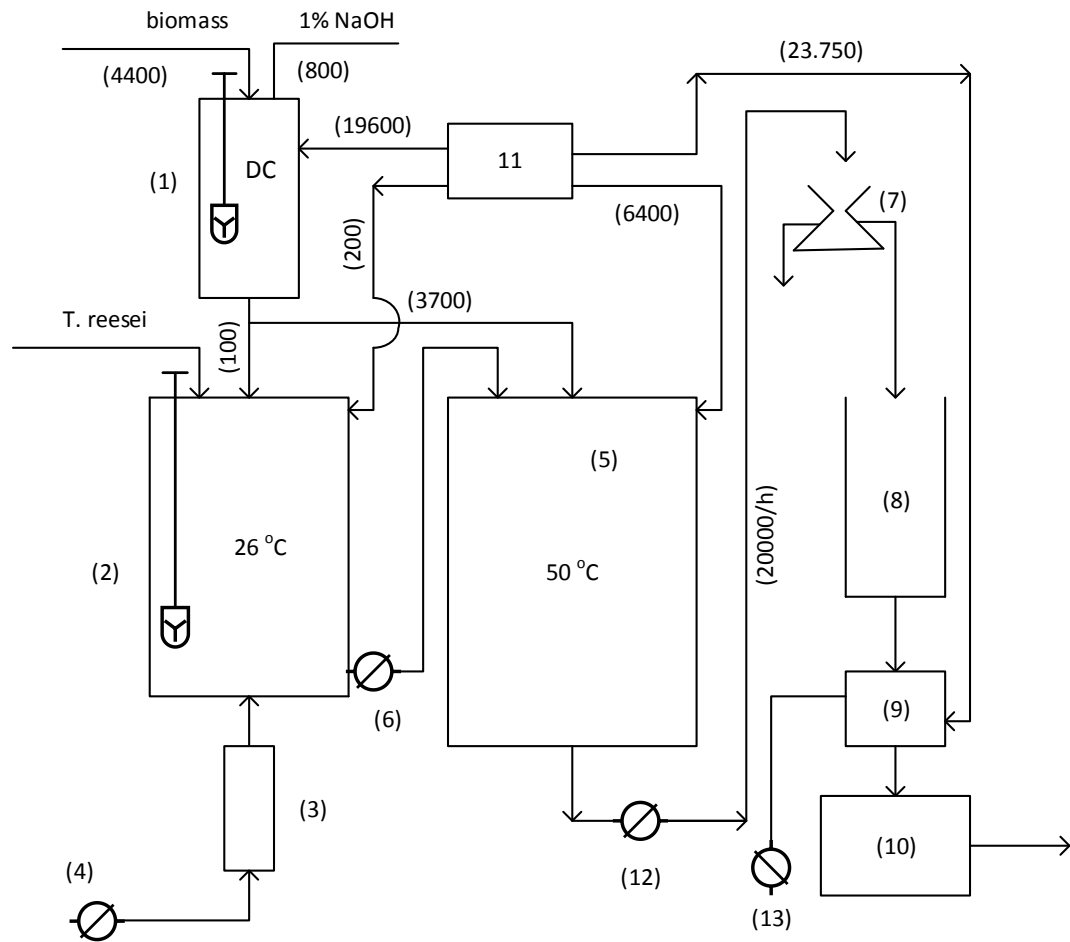












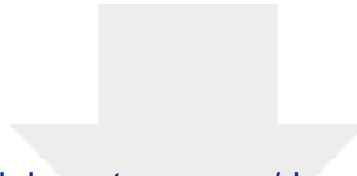
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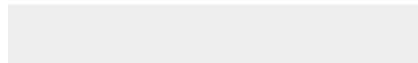
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Pump	4 m ³ /h	2,000
Centrifugal separator	20 m ³ /h	150,000
Tank for CHNTs solution	100,000 L	30,000
Condenser	3.3 m ³ /h	300,000
Freeze dryer	6000 Kg water/day	500,000
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Water requirement	40
Consumables	205
Investment payments	156
Total	2731



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Supplementary Interactive Plot Data (CSV)
SUPPLEMENTARY MATERIALS.docx



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Declaration of interests

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

The authors declare the following financial interests/personal relationships which may be considered as potential competing interests:

CRedit authorship contribution statement

Athanasia Panitsa: Methodology, Validation, Investigation, Writing - original draft, Visualization. **Theano Petsi:** Methodology, Writing - review & editing. **Eleana Kordouli:** Methodology, Validation. **Poonam S. Nigam:** Result-analysis for writing-second draft, editing. **Maria Kanellaki:** Supervision. **Athanasios A. Koutinas:** Conceptualization, Writing - original draft, Project administration, Funding acquisition.