

Direct Formation of Copper Nanoparticles from Atoms at Graphitic Step-Edges Lowers Overpotential and Improves Selectivity of Electrocatalytic CO₂ Reduction

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Supplementary figures

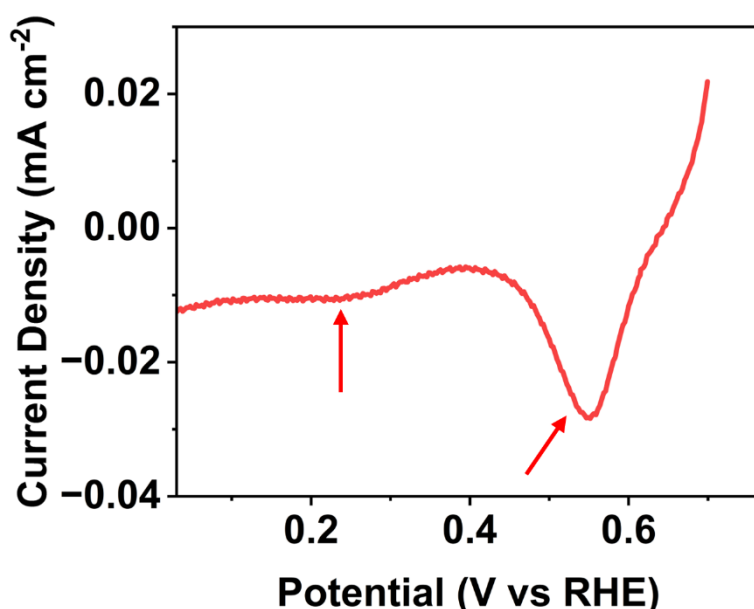


Figure S1. LSV of as-sputtered Cu/GNF at a scan rate of 10 mV s⁻¹ measured in 0.1 M KHCO₃, illustrating two copper reduction peaks.

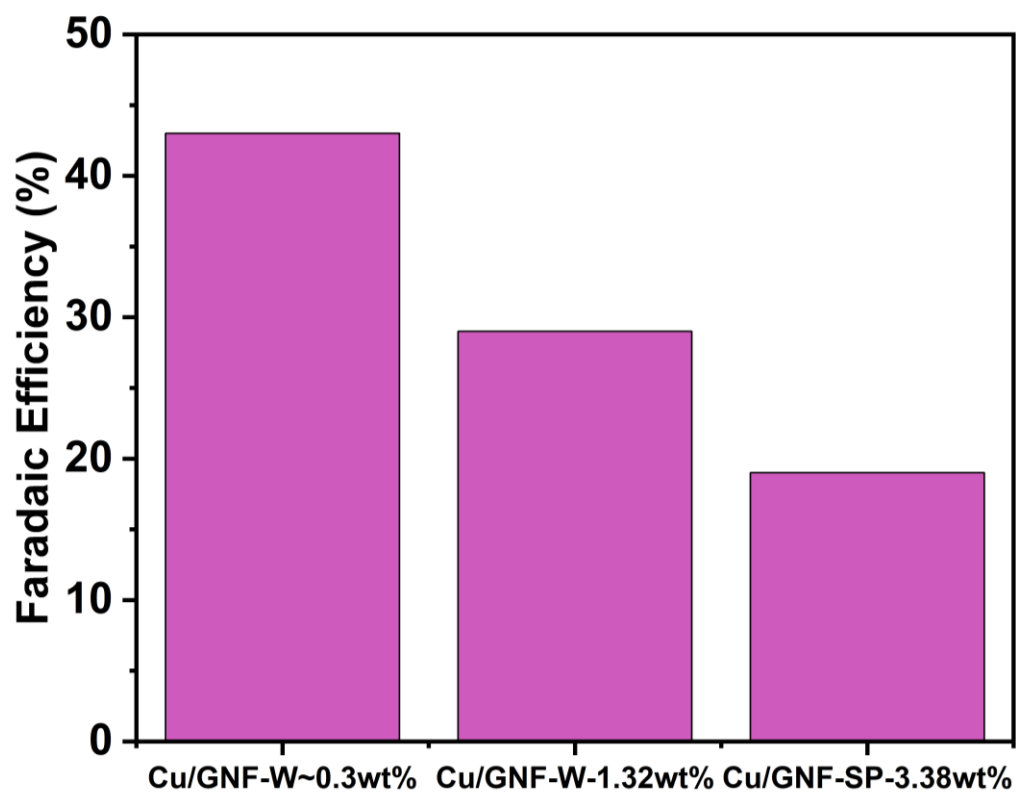


Figure S2. FE of formate at -0.38 V vs RHE obtained for wet chemistry prepared Cu/GNF catalysts and higher weight loading of the sputtered sample. (W represents wet chemistry prepared and SP sputter prepared).

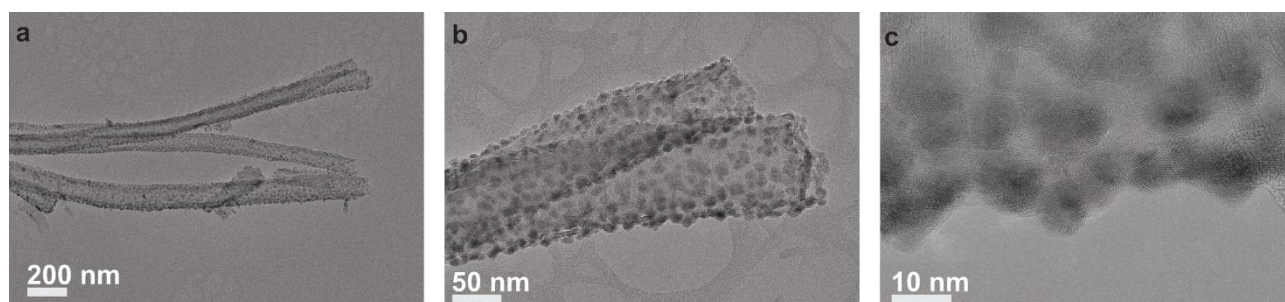


Figure S3. a-c) HR-TEM of 3.38 wt.% weight loading of Cu on GNF

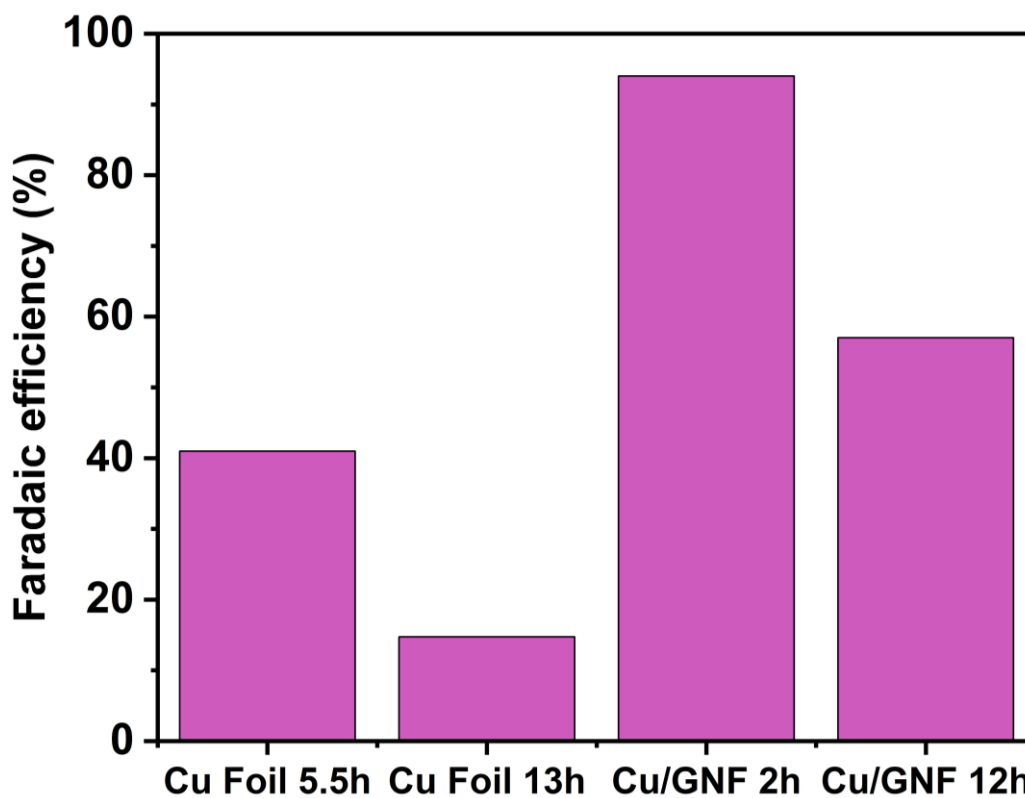


Figure S4. FE of formate of Cu foil after 5.5 h and 13 h vs. GNF/Cu after 2 h and 12 h at -0.38V vs RHE

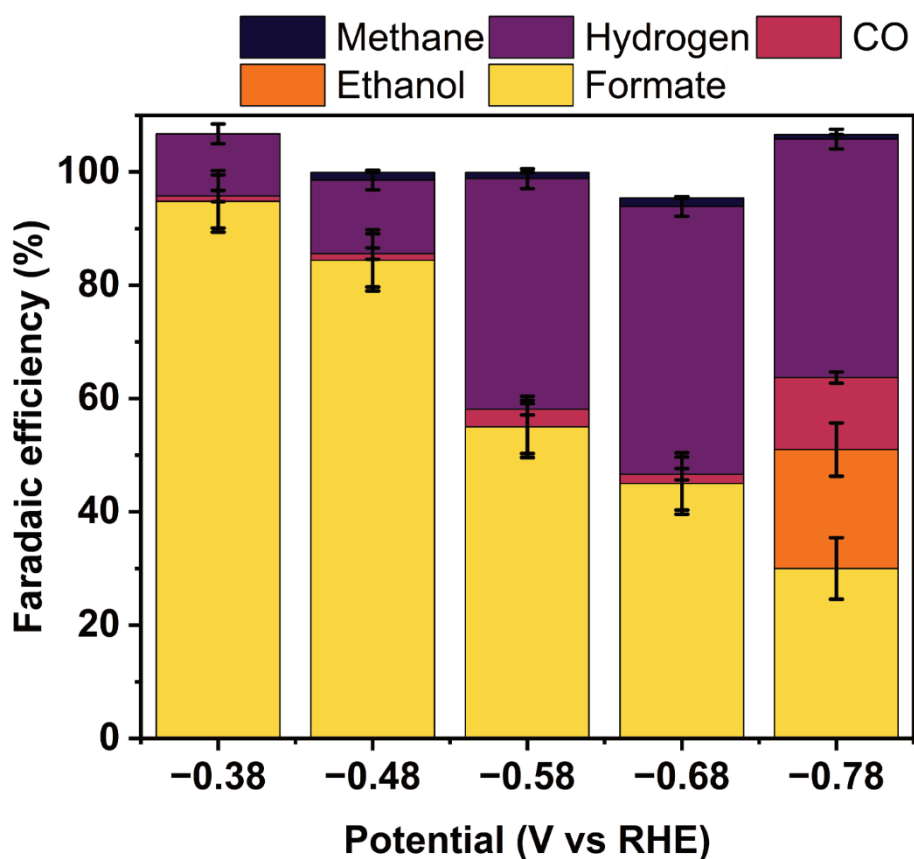


Figure S5. Faradaic efficiency including detectable gas products from -0.38 to -0.78 V vs RHE.

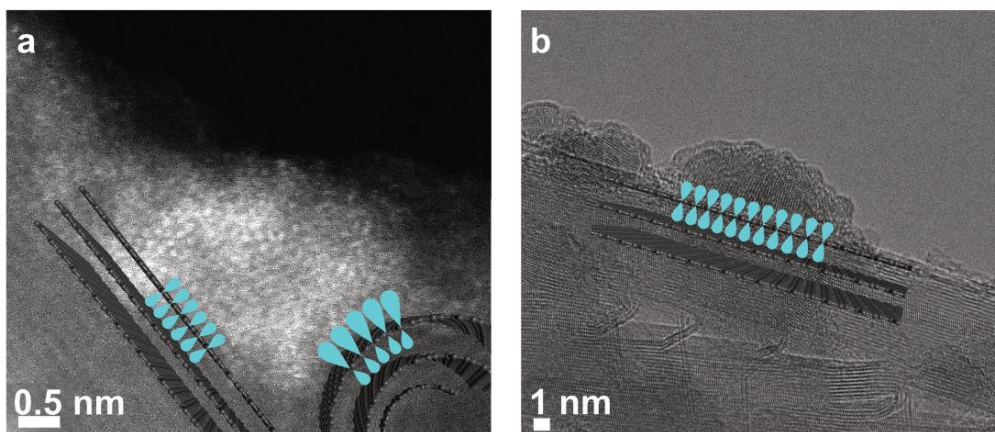


Figure S6. Schematic representation of the carbon π orbital interactions with surface Cu on PR-24 (with external step edges (a) and PR-19 (without external step edges) GNFs (b)

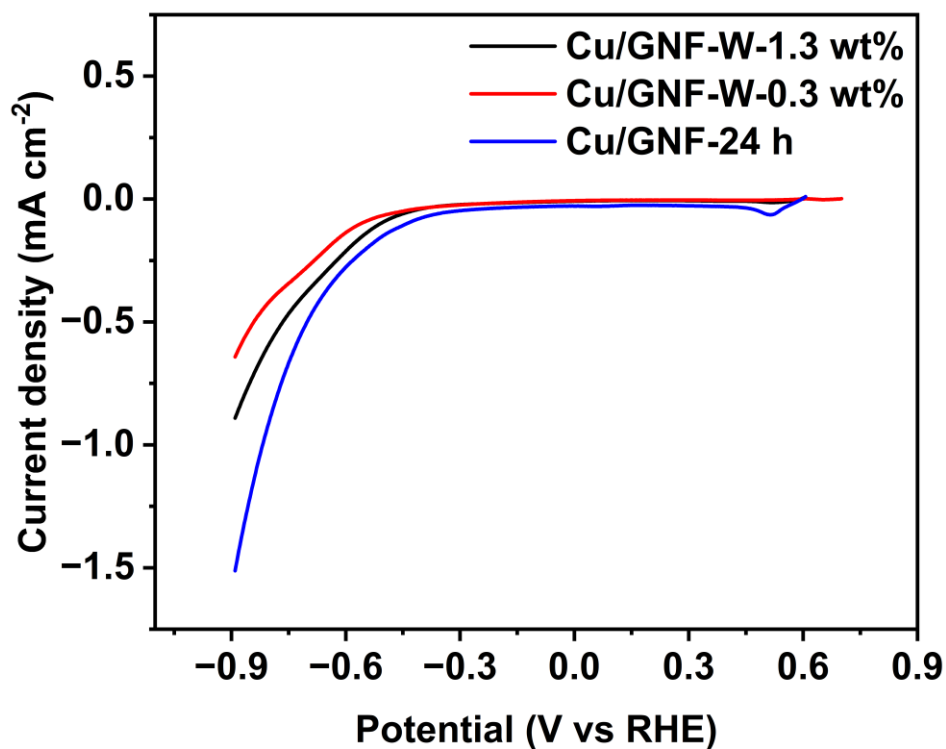


Figure S7. LSV of wet chemistry prepared Cu/GNF measured in 0.1 M KHCO_3 sweeping from +0.6 to -0.88 V vs RHE at a scan rate of 10 mV s^{-1} , where W denotes wet chemistry prepared.

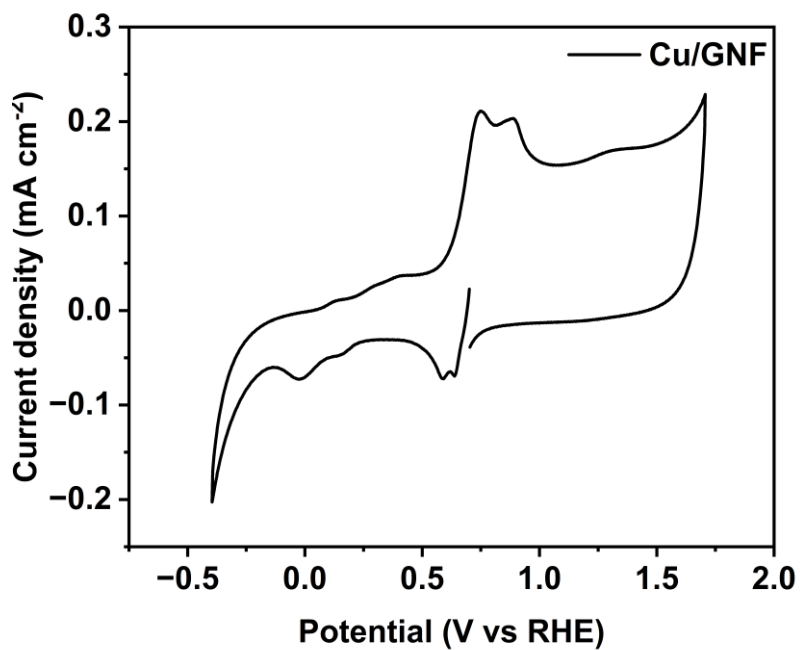


Figure S8. Post-reaction (24 h) CV of Cu/GNF from 1.8 to -0.48V vs RHE at a scan rate of 10 mV/s in reaction electrolyte (0.1 M KHCO₃).

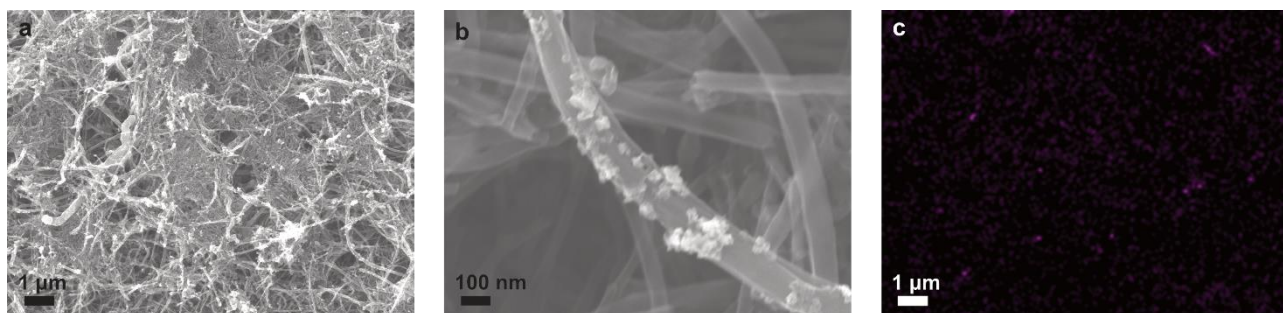


Figure S9. a and b) SEM of the used catalyst after 24 hours at -0.37V vs RHE. c) EDX-mapping of Cu of a).

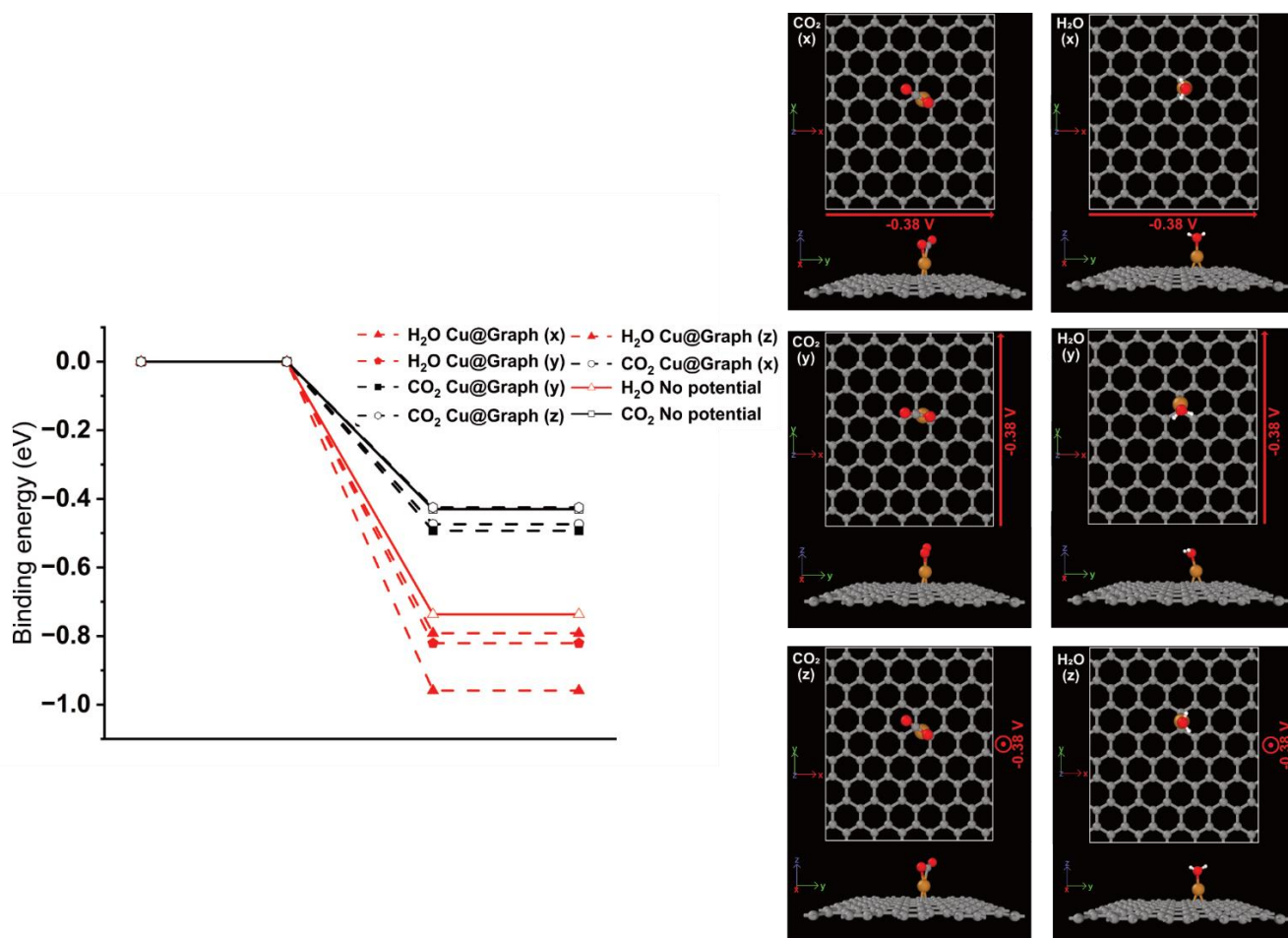


Figure S10. The binding energy of CO₂ and H₂O on Cu atom adsorbed on graphene under external applied field of -0.38 V along the X, Y and Z-axis.

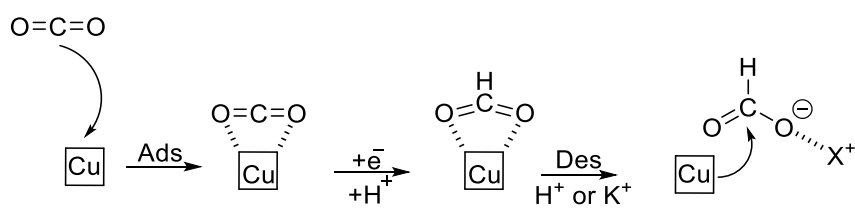


Figure S11. Proposed mechanism(s) for formate on NCs of Cu

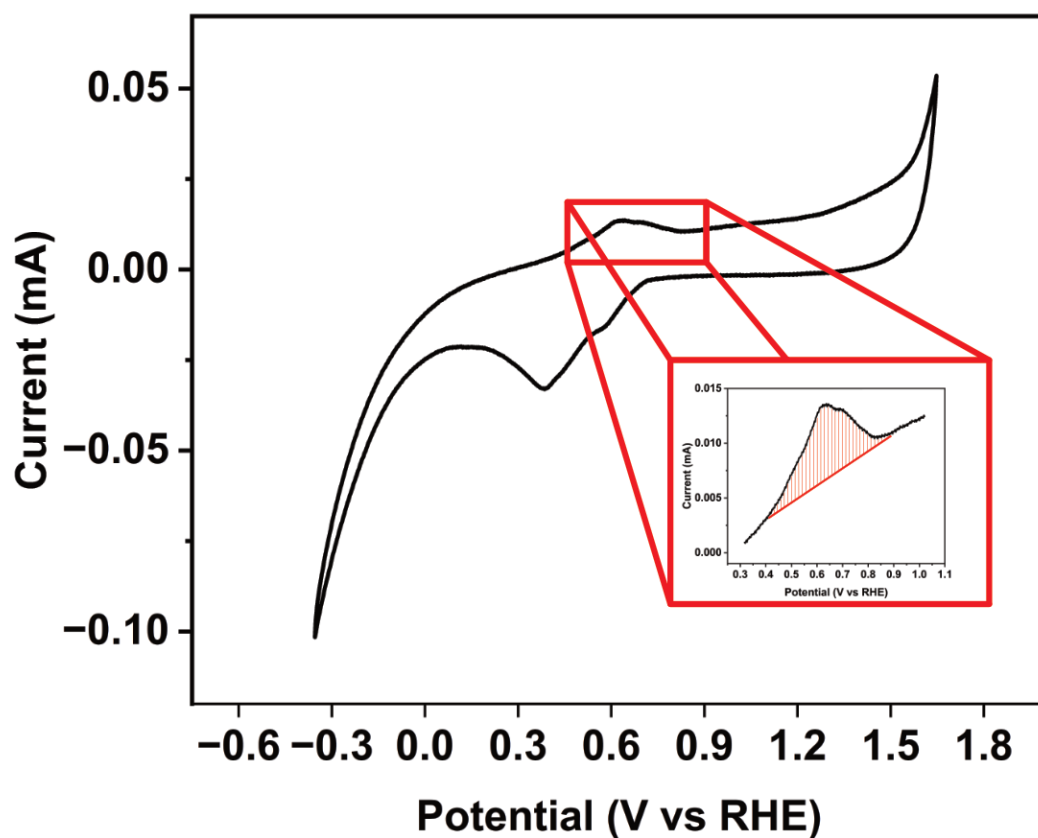


Figure S12. Integration of Cu oxidation on the anodic sweep of a CV sweeping at 10 mV/s, in 0.1 M KHCO_3 from -0.36 V to 1.65 V vs RHE.

Table S1. Comparison of PR-19 (no step-edges) and PR-24 GNFs FE for formate

| Catalyst | Potential (V vs RHE) | Faradaic efficiency (%) |
|------------------------|----------------------|-------------------------|
| (PR-19) | -1.18 | 1.03 |
| GNF with no step-edges | -0.88 | 3.12 |
| | -0.38 | 5.43 |
| (PR-24) | -1.18 | 10.5 |
| GNF with step-edges | -0.88 | 22.8 |
| | -0.38 | 94.8 |

Table S2. Cu p_{3/2} XPS results for Cu/GNF materials, including % peak area.

| Sample | Oxidation State | Binding Energy (eV) | Peak Area | % Peak Area |
|-------------|-------------------------------------|---------------------|-----------|-------------|
| Cu/GNF | (Cu ⁰ +Cu ^I) | 932.82 | 4512 | 40.8 |
| | Cu ^{II} | 934.79 | 4006 | 36.2 |
| | Sat2 | 941.83 | 1537 | 13.9 |
| Cu/GNF-24 h | Sat1 | 944.33 | 1000 | 9.1 |
| | (Cu ⁰ +Cu ^I) | 932.86 | 2062 | 52.6 |
| | Cu ^{II} | 934.81 | 1322 | 33.7 |
| | Sat2 | 942.92 | 503 | 12.8 |
| | Sat1 | 944.69 | 161 | 0.9 |

Cu/GNF

(Cu⁰+Cu^I) = 33.7 % // (Cu^{II}) = 66.3%

Cu/GNF-24 h

(Cu⁰+Cu^I) = 60.4 % // (Cu^{II}) = 39.6%

Table S3. Comparison of literature Cu-based electrocatalyst with the present Cu/GNF

| Catalyst | Year | Electrolyte | Potential (V vs RHE) | FE of formate (%) | Reference |
|---|------|-------------------------|----------------------|-------------------|-----------|
| Cu/GNF | 2024 | 0.1 M KHCO ₃ | -0.38 | 94 | This work |
| Cu/N-Doped porous Carbon | 2023 | 0.1 M KHCO ₃ | -0.70 | 52 | 1 |
| Cu/CuO _x /SnO _x on porous carbon | 2023 | 0.5 M KHCO ₃ | -1.1 | 69 | 2 |
| Cu ₁ Bi ₂ Aerogel | 2022 | 0.5 M KHCO ₃ | -0.90 | 96 | 3 |
| Cu-FTGDE | 2024 | 0.5 M KHCO ₃ | -0.90 | 76 | 4 |
| Cu ₂ SnS ₃ | 2023 | 0.1 M KHCO ₃ | -1.20 | 92 | 5 |
| SU-101-Cu@2.5C | 2023 | 0.5 M KHCO ₃ | -0.96 | 95 | 6 |
| Cu/Bi ₂ S ₃ -2.67%-N ₂ | 2023 | 0.5 M KHCO ₃ | -0.80 | 94 | 7 |
| Pd ₇₃ Cu ₂₇ | 2023 | 0.5 M KHCO ₃ | -0.56 | 81 | 8 |
| Cu-Pd/MXene | 2023 | 0.1 M KHCO ₃ | -0.50 | 79 | 9 |
| Bi ₉ Cu ₁ | 2023 | 0.5 M KHCO ₃ | -0.80 | 98 | 10 |

Supplementary Note 1

Gas product calculations. Example for H₂

$$FE(\%) = \frac{Q_{product}}{Q_{total}} \times 100 = \frac{n \times F \times f_{gas} \times t \times Product_{moles}}{Q_{total} \times 24.4 \times 10^3} \times 100$$
$$FE = \frac{2 \times 96485 \text{ C mol}^{-1} \times 5 \text{ ml min}^{-1} \times 60 \text{ min}}{24.4 \times 10^3 \text{ mL} \times 29.69 \text{ C}} \times \left(\frac{11.36 \times 10^{-6} \text{ mol}}{0.1 \text{ ml}} \times 45 \text{ ml} \right) \times 100$$
$$FE = \frac{57891000 \times 5.11 \times 10^{-3}}{7.24 \times 10^5} \times 100$$
$$FE = \frac{2.96 \times 10^5}{7.24 \times 10^5} \times 100 = 40.88 \%$$

Where n number of electrons for hydrogen generation, F is Faraday constant, f_{gas} is the flow rate of CO₂, t is time of injection, $Product_{moles}$ is the amount of moles of product, 24.4×10^3 is the molar volume of 1 mole of gas and Q_{total} is the charge passed after time t.

Supplementary Note 2

Liquid product calculations. Example for Formate

Concentration in NMR tube:

$$Concentration = 0.333 \times \frac{(0.0228 \times 6)}{(1 \times 3)} = 0.015 \text{ mM}$$

Concentration in 0.4 mL aliquot:

$$Concentration = \frac{(0.015 \times 0.000488)}{0.0004} = 0.018 \text{ mM}$$

Moles in H-cell:

$$Moles = \frac{(0.018 \times 0.035)}{1000} = 6.48 \times 10^{-7} \text{ moles}$$

Charge passed to form product:

$$Charge = 6.48 \times 10^{-7} \times 96485.33 \times 2 = 1.25 \times 10^{-1} \text{ C}$$

Faradaic efficiency:

$$FE = \frac{1.25 \times 10^{-1}}{1.32 \times 10^{-1}} \times 100 = 94.7 \%$$

Supplementary References:

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