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Capacitive Deionization of Saline Water by Using MoS₂-Graphene Hybrid Electrodes with High Volumetric Adsorption Capacity

Jinlong Han,^{§,†} Tingting Yan,^{§,†} Junjie Shen,[‡] Liyi Shi,[†] Jianping Zhang[†] and Dengsong Zhang^{*,†}

4 [†] Department of Chemistry, College of Sciences, State Key Laboratory of Advanced Special Steel,

5 Research Center of Nano Science and Technology, School of Materials Science and Engineering,

6 Shanghai University, Shanghai 200444, PR China.

⁷ [‡] Department of Chemical Engineering, University of Bath, Bath BA2 7AY, UK.

8 * Corresponding authors: E-mail: <u>dszhang@shu.edu.cn</u>.

9 § J.H. and T.Y. contributed equally to this work.

ABSTRACT: Capacitive deionization (CDI) has received wide attention as an emerging water 10 treatment technology due to its low energy consumption, low cost and high efficiency. However, the 11 conventional carbon electrode materials for CDI have low densities, which occupy large volumes and 12 13 are disadvantageous for use in limited space (e.g., in household or on offshore platforms). In order to miniaturize the CDI device, it is quite urgent to develop high volumetric adsorption capacity (VAC) 14 electrode materials. To overcome this issue, we rationally designed and originally developed high VAC 15 MoS₂-graphene hybrid electrodes for CDI. It is interesting that MoS₂-graphene hybrid electrode has a 16 much higher NaCl volumetric adsorption capacity of 14.3 mg/cm³ with a gravimetric adsorption 17 capacity of 19.4 mg/g. It has been demonstrated that the adsorption capacity is significantly enhanced 18 due to the rapid ion transport of MoS₂ and high electrical conductivity of graphene. In-situ Raman 19 spectra and high-angle annular dark-field scanning transmission electron microscopy tests 20 demonstrated a favorable Faradaic reaction, which was crucial to enhancing the NaCl volumetric 21 adsorption capacity of MoS₂-graphene hybrid electrode. This work opens a new avenue for 22

23 miniaturizing future CDI devices.

24 INTRODUCTION

With the growth of population and the development of industry, human beings consume a large amount of fresh water resources.¹ The widespread water scarcity and water contamination problems are seriously increasing across the world, threatening human health and ecological integrity.²⁻⁵ In coastal areas, desalination of saline water is an important way to obtain fresh water.⁶ Conventional desalination methods include reverse osmosis thermal distillation and electrodialysis.⁷⁻⁹ They have demonstrated a variety of disadvantages in practical applications, such as high energy consumptions and high economic costs.¹⁰

As an emerging water treatment technology, capacitive deionization (CDI) has gained increasing 32 attention due to its prominent advantages, such as high efficiency, low cost, low energy consumption 33 and easy operations and ease of maintenance.¹¹⁻¹³ The principle of CDI is analogous to that of the 34 electrical double-layer capacitor:¹⁴ When exposed to an external electric field, the charged ions in the 35 feed water move towards the oppositely charged electrode by electrostatic attraction and are adsorbed 36 37 and/or trapped on the surface of electrodes accompanied by simultaneous energy storage, thus the deionized water is produced in the outlet. When the electric field is reversed or the electrodes were 38 short-circuited, the ions adsorbed in the electrodes are released, accompanied by the release of energy 39 stored in the electrodes, therefore the electrodes are regenerated. Various CDI models and techniques, 40 such as flow electrode capacitive deionization, membrane capacitive deionization, faradaic CDI and 41 hybrid CDI have attracted increasing attention in the last decade.^{9,15-17} 42

Electrode materials are vital for the CDI performance. Key features of an excellent electrode
material include high electrical conductivity, high adsorption capacity, reasonable pore structure, high

chemical and mechanical stability, environmentally friendly, and favorable water wettability.¹⁸ 45 Traditional electrode materials used in CDI, including activated carbon (AC), porous carbon, carbon 46 fibers, carbon cloths, carbon nanotubes and graphene have been extensively studied due to their high 47 chemical stability, high electrical conductivity and high adsorption capacity.¹⁹ In recent years, some 48 materials with pseudocapacitance such as TiO₂, MnO₂, MoS₂, some molybdate and phosphate 49 attracted a lot of attentions.²⁰⁻²² Despite great efforts have been devoted to preparing novel CDI 50 electrode materials,²³⁻²⁵ most of current studies are focused on the enhancement of the gravimetric 51 adsorption capacity (GAC, mg/g) while little attention has been paid to the enhancement of the 52 volumetric adsorption capacity (VAC, mg/cm³). Traditional carbonaceous electrodes are relatively low 53 in density, such as only 0.4-0.6 g/cm³ for activated carbon and 1-2 g/cm³ for multiwall carbon 54 nanotubes.²⁶ The utilization of low density materials leads to its low VAC, which is unfavorable when 55 56 the CDI devices are used in a limited space (e.g., in household or on offshore oil/gas platforms).²⁷ Therefore, enhancing the VAC of the CDI electrodes is a major objective for future CDI development. 57 MoS₂ is one of the most interesting two-dimensional layered materials, in which two layers of sulfur 58 atoms are sandwiched by a layer of molybdenum atoms. Each three-layer structure is connected by a 59 weak Van Der Waals force, which gives MoS₂ a variety of fascinating properties such as large surface 60 area, high density and fast ionic conductivity.²⁸ Specifically, the density of MoS₂ is around 4-5 g/cm³, 61 which is much higher than that of carbon materials.²⁹ Combining the high electrical conductivity of 62 graphene with the high density of MoS₂ may result in a highly conductive and compact electrode 63 material for CDI. 64

Herein, we rationally designed and originally developed a novel hybrid MoS₂-graphene electrode
 for CDI applications (Figure 1a and 1b). The MoS₂-graphene electrode showed a high NaCl adsorption

67 capacity (VAC_{NaCl}) as well as a high NaCl adsorption capacity (GAC_{NaCl}), as a result of the high 68 electrical conductivity of graphene and the rapid ion transport of MoS₂. This study reveals a new 69 avenue for miniaturizing future CDI devices.

70 **EXPERIMENT**

Preparation. Graphene oxide (GO, 99.5%, Graphene-king Company, Shanghai, China), ammonium 71 molybdate tetrahydrate ((NH₄)₆Mo₇O₂₄·4H₂O) and thiourea were purchased from Aladdin (Shanghai, 72 China). All the chemicals were analytically pure and not purified further. MoS2-graphene hybrid 73 electrodes were synthesized through a simple *in-situ* growth strategy (Figure 1b). Typically, 1.12 g 74 75 thiourea and 40 mg graphene oxide (dispersed in DI water, 2 mg/mL) were dissolved in 75 mL water under vigorous stirring to make a homogenous mixture. Then 4 g (NH₄)₆Mo₇O₂₄·4H₂O was added into 76 the mixture under stirring for 30 min followed by transferring into the 100 mL Teflon-lined stainless 77 78 autoclave and hydrothermally treated at 170 °C for 12 h. Afterward, the sediment was separated by suction filtration and washed by absolute ethanol and DI water followed by drying at 60 °C at ambient 79 air. At last, the resultant powder was calcined at 600 °C with a ramping rate of 5 °C /min under a 80 81 flowing argon atmosphere. Samples with graphene oxide additive amount of 0, 40, 60, 80, 100 and 200 mg were named by MoS₂, MG-0.8, MG-1.2, MG-1.6, MG-1.9 and MG-3.8, respectively. 82

Characterization. Scanning electron microscope (SEM, Hitachi S-4800) and transmission electron microscope (TEM, JEM 2100) were used to observe the morphological and structural properties of the samples. The phase compositions were determined using the X-ray diffractometer (XRD, Cu Ka, 40 kV, 20 mA). Raman spectroscopy were investigated by a spectrometer with a 633 nm Ar⁺ laser and *in-situ* Raman spectra of whole cyclic voltammetry (CV) cycle between 0.5 V and - 0.5 V were conducted on a Raman spectrometer (HORIBA scientific, LabRAM HR Evolution, France)

with a 633 nm laser. Nitrogen isothermal adsorption-desorption curves were investigated (Autosorb-89 IQ2, America). The specific surface area and the pore size distribution were determined by the 90 Brunauer-Emmett-Teller (BET) method and the Barrett-Joyner-Halenda (BJH) and density 91 Functional Theory (DFT) model, respectively. Water wettability was evaluated by drop shape analysis 92 using Kruss, DSA100 instrument. Electrochemical performance was evaluated through an 93 electrochemical workstation (CHI 660D, Chenhua, Shanghai). The working electrode was fabricated 94 through mixing of polytetrafluoroethylene (PTFE) aqueous dispersion and active material with a ratio 95 of 1:9 in weight and shaped into 1 cm square film. The CV and galvanostatic charge-discharge (GCD) 96 97 curves and electrochemical impedance spectroscopy (EIS) were measured in a 0.5 M NaCl solution with a three-electrode system. The calomel electrode and graphite film serve as reference electrode 98 and counter electrode, respectively. The capacitance is calculated by the equation (1) 99

$$C = \frac{\int IdV}{2mu\Delta V} \tag{1}$$

101 Where *C* is the capacitance (F/g), *I* is the response current density (A), *m* is the mass of active material 102 (g), *v* is the scanning rate (V/s), and ΔV is the applied voltage window during the cyclic voltammetry 103 test (V). The proportion of contribution of capacitive charge and the diffusion-controlled charge were 104 calculated according to the equation (2).³⁰

 $i(V) = k_1 \iota$

$$i(V) = k_1 v + k_2 v^{0.5} \tag{2}$$

Where the *i* is the current (A), the *v* is the scanning rate (mV/s), k_1 and k_2 are constant values at a fixed potential. k_1v is related to the capacitive current raised from electrical double layer (EDL) and $k_2v^{0.5}$ is related to diffusion-controlled charge.

109 **Batch-Mode CDI Experiments.** The electrode for batch-mode CDI experiments was 110 fabricated through adequate mixing of the PTFE, conductive carbon black and as-prepared active

material with a ratio of 1:1:8 in weight, then was shaped into 65 mm square film and casted onto the 111 graphite film current collector. An asymmetric electrode system was assembled using as-prepared 112 electrode and graphite film (GF) as the working electrode and the counter electrode (GFIMG-1.6 113 electrode pairs), respectively. The other asymmetric electrode was assembled using as-prepared 114 electrode and graphite film loaded with activated carbon as the working electrode and the counter 115 electrode (ACIIMG-1.6 electrode pairs), respectively. The homemade device (Figure 1a) was used to 116 examine the salt adsorption performance as demonstrated in previous work by our group.^{31,12} The two 117 CDI electrodes was separated by placing a spacer between them. A 50 mL NaCl solution was driven 118 119 cyclically through the electrodes via a peristaltic pump. A conductivity meter (SevenMulti, METTLER TOLEDO, America) was used to monitor the conductivity of the NaCl solution online. When it is 120 necessary to compare the variations of solution conductivity in different batch-mode test, the initial 121 122 solution conductivity is normalized just for comparative purposes to eliminate the system error. In this work, graphite film loaded with as-prepared material was used as cathode, graphite film or graphite 123 film loaded with activated carbon was used as anode. The GAC was calculated in theory by the 124 equation (3): 125

132

$$GAC = GAC_T - GAC_{NA} \tag{3}$$

Where the *GAC* is gravimetric adsorption capacity (mg/g), the *GAC_T* is the total *GAC* obtained by CDI tests of the whole electrodes (mg/g), the *GAC_{NA}* is the premeasured *GAC* of non-active materials (mg/g). For CDI test with GFIMG-1.6 electrode pairs, Na⁺ ions gravimetric adsorption capacity (*GAC_{Na}*) was used to evaluate the ability of deionization of active materials, which was calculated by the equation (4) as follow.

$$GAC_{Na} = \frac{0.394(C_{NA} - C_T)V}{M}$$
(4)

Where 0.394 is the mass fraction of sodium in NaCl, C_{NA} is the NaCl aqueous solution concentration during the desalination test of non-active material (mg/L) (Figure S1), C_T is the NaCl aqueous solution concentration during the desalination test of the as-prepared electrodes (mg/L), M is the quality of asprepared electrode material (g) and V is volume of NaCl solution (L). The thickness of active material film is calculated by follow equation (5):

138

142

$$T_{af} = T_t - T_{cc} \tag{5}$$

Where T_{af} is active material film thickness (µm), T_t is average total thickness (µm), T_{cc} is average current collector (graphite film) thickness (µm). Both the T_{cc} and T_t are measured by micrometer (Figure S3). The Na⁺ volumetric adsorption capacity (*VAC_{Na}*) was calculated by the equation (6):

$$VAC_{Na} = \frac{GAC_{Na} \times M}{T_{af} \times a} \tag{6}$$

Where *a* is the area of active electrode film on the current collector (cm²), respectively. For the CDI test with ACIMG-1.6 electrode pairs, the GAC_{NaCl} was calculated by the equation (7) as follow.

145 $GAC_{NaCl} = \frac{(C_{NA} - C_T)V}{m_t}$ (7)

146 Where m_t is the quality of total mass both cathode and anode electrode material (g). The NaCl *VAC_{NaCl}* 147 was calculated by the equation (8):

148
$$VAC_{NaCl} = \frac{GAC_{NaCl} \times m_t}{aT_{af} + bT_{AC}}$$
(8)

Where *b* is activated carbon film area (cm²), T_{AC} is activated carbon film thickness (cm). The T_{AC} was calculated adopted similar method with T_{af}. Average Na⁺ adsorption rate (ASAR_{Na}) (mg/cm³/min) was calculated by equation (9):

152
$$ASAR_{Na} = \frac{0.394V \int_0^t (C_{NA}(t) - C_T(t))dt}{T_{af} \times a \times t}$$
(9)

153 Where $C_{NA}(t)$ and $C_T(t)$ is instant concentration of the NaCl aqueous solution during the deionization

(mg/L), t is the time of deionization (min). During the regeneration of the electrode, the external

direct voltage was removed and the work electrode was directly connected with the counter electrodeby a copper wire.

The regeneration tests were conducted at a flow rate of 60 mL/min and a direct voltage of 1.2 V.
The initial conductivity of the NaCl solution was 200 µS/cm. When the electrodes were regenerated,
they were connected by wire directly to release the adsorbed ions.

160

RESULTS AND DISCUSSION

Structure and Composition Analysis. The morphologies of the obtained materials were 161 demonstrated by TEM and SEM images. Figure 1c-d show the SEM images of the MG-1.6. There are 162 a large number of MoS₂ pleats on the surface of the particles and these protrusions are uniform and 163 interlaced in a flaky shape, which is advantageous for increasing the specific surface area. According 164 to the TEM (Figure 1e-1f) and HRTEM (Figure 1g) images of MG-1.6, it can be clearly observed that 165 166 a large number of MoS₂ sheets are homogenously distributed on the surface of the graphene, which is conducive to increase the conductivity of electrode. The lattice spacing was calculated to be 0.68 nm 167 (Figure 1g), corresponding to the (002) lattice plane of the hexagonal MoS₂.³² The thickness of the 168 MoS₂ layer of MG-1.6 is calculated to be 9 nm corresponding to layers number of 14, which contributes 169 to increase conductivity of the MoS₂-graphene hybrid electrode. It was found that as the additive 170 amount of graphene oxide increases, the agglomeration of the sheet-like MoS₂ on graphene is 171 alleviated and the sheet becomes smaller with a better dispersion (Figure S2). When the additive 172 amount of graphene oxide is more than 1.9 wt%, the MoS₂ sheets cannot be clearly distinguished 173 (Figure S2f). This result is possibly due to the fact that graphene provides nucleation sites for the 174 formation of MoS₂,^{33,34} and an increase in the amount of graphene makes the nucleation rate surpass 175 the growth rate, resulting in a reduction in the size of MoS₂ sheets. However, too small MoS₂ crystals 176

are not beneficial to preventing graphene stacking. Conversely, the highly agglomerated MoS₂ is
unfavorable for mass transfer, because the number of adsorption sites is limited.

The phase properties of different samples were examined by XRD (Figure 2a). The obvious 179 diffraction peaks located at 13.7°, 33.6° and 59.9° correspond to the (002), (100) and (008) planes of 180 hexagonal MoS₂ (JCPDS, No. 37-1492), respectively, indicating good crystalline nature of MoS₂. That 181 is favorable to the chemical stability of electrode. Actually, the peaks located at 26°, 37.0° and 53.5° 182 in the Figure 2a are corresponding to (011), (020) and (022) planes of MoO₂ (JCPDS 65-5787).³⁵ MoO₂ 183 is produced because the (NH₄)₆Mo₇O₂₄·4H₂O is excessive and the thiourea is insufficient. The 184 excessive molybdate ions were transformed into MoO₂. As the electrical resistivity of MoO₂ ($10^{-5} \Omega$) 185 cm⁻¹) is much lower than that of MoS₂ (~1 Ω cm⁻¹), therefore MoO₂ is beneficial for conductivity of 186 the as-prepared materials.^{36,37} 187

188 The specific surface areas calculated from N₂ adsorption-desorption isotherms (left of Figure 2b) for MG-0.8, MG-1.2, MG-1.6, MG-1.9, MG-3.8 are 27.2, 28.9, 37.9, 35.3 and 34.2 m²/g, respectively. 189 The results implied that the content of graphene affects the specific surface area significantly. Low 190 191 content of graphene makes MoS₂ agglomerated and excessive graphene makes itself stacked. The hysteresis curves include a hysteresis loop at a high-pressure stage, and the area of the hysteresis loop 192 is related to the pore volume.³⁸ According to the pore size distribution profiles (right of Figure 2b and 193 Figure S4), MG-1.6 has the large portions of mesopores, indicating their superior mass transfer 194 capacities. Moreover, the good hydrophilicity of MG-1.6 has been demonstrated (Figure S5), which 195 favors the CDI process for the practical applications. 196

197 The Raman spectra were conducted to examine the structure and topology of the MoS_2 -graphene 198 and the layer number (Figure 2c and 2d). The peaks located at 378 cm⁻¹ and 405 cm⁻¹ are corresponding

to E¹_{2g} and A_{1g} peaks, respectively.²⁰ E¹_{2g} peak is assigned to the in-plane displacement in Mo and S 199 atoms and A1g is assigned to the out-plane symmetric displacement of S atom along the c-axis.³⁹ As 200 shown in Figure 2d, a slight blue-shift of A1g is found, indicating the layer number of MoS2 201 decreasing,^{40,41} which accounts the effect of inhibition on layer number of MoS₂ by graphene. The 202 peak located at around 1360 cm⁻¹ and 1580 cm⁻¹ are corresponding to the D and G peaks of graphene 203 (Figure 2c), which arise from the sp³-hybridized carbon and the sp²-hybridized carbon.⁴² The 204 increasing intensity of D and G peaks indicates the increase of graphene content, moreover, the D peak 205 is larger than G peak demonstrating the small degree of graphitization. 206

Electrochemical Performance. The GCD test was implemented to examine the capacitance 207 of the as-prepared samples (Figure 3a). The results show that MG-1.6 has the longest discharge time 208 at 0.2 A/g, implying that it possesses the largest capacitance among all the electrodes. The sample MG-209 210 1.6 was tested at different current densities (Figure S6a). The result shows that it keeps a long discharge time of 150 s at a large current density of 1.0 A/g. The extent of IR drop is positively related to the 211 inner electrical resistance of the electrodes.^{12,43} The IR drop of MG-1.6 displays the smallest IR drop 212 213 (the inset of Figure 3a), indicating that it has the smallest inner electrical resistance. The result is due to the preferable distribution of MoS₂ particles of MG-1.6 on the graphene, ensuring a high electrical 214 conductivity and a small internal resistance. The IR drops at different current densities are shown in 215 Figure S6b. The result confirms that the IR drop increases linearly with the increase of current density, 216 which is attributed to the inadequate discharge in the EDL at the onset of discharge. A superior charge-217 discharge performance and a good cyclic stability of 10 000 cycles are obtained for MG-1.6 electrode 218 (Figure 3d). 219

220 The CV test for exploring the electrochemical behavior in a 0.5 M NaCl solution shows the

rectangular-like closed curve of MG-1.6 (Figure S6c), suggesting good capacitor characteristics.⁴⁴ As 221 calculated from the area of the rectangular curves, the capacitances of MG-1.6 is 146.1 F/g at a 222 223 scanning rate of 5 mV/s, which is higher than other contrast samples (Figure S6d), implying remarkable adsorption capacity. The capacitances of MG-1.6 at different scanning rates are shown in 224 Figure S6e. The MG-1.6 still has a capacitance of 47.9 F/g even at a high scan rate of 50 mV/s, which 225 is due to the good electrical conductivity of MG-1.6. Two redox peaks at 1 mV/s (Figure S6f) 226 demonstrates the existence of a redox process. The proportion of contribution of capacitive charge and 227 the diffusion-controlled charge were calculated according to the equation (2). CV curves at 0.2 mV/s 228 229 and 0.5 mV/s have been measured, respectively. Based-on the equation (2), at a given potential P, two known different current values i_1 and i_2 are obtained at two scanning rates v_1 (0.2 mV/s) and v_2 (0.5 230 mV/s), thus obtaining a binary equations as follow. 231

232
$$i_1(P) = 0.2k_1 + \sqrt{0.2}k_2$$
 (10)

233
$$i_2(P) = 0.5k_1 + \sqrt{0.5}k_2$$

 k_1 and k_2 at *P* potential can be obtained by solving the above binary equations consisting equation (10) and (11). A CV cycle contains a series of potential values, so a series of k_1 and k_2 values can be obtained. For the same material, k_1 and k_2 are fixed at a given potential. Therefore, at the scanning rate of 0.2 mV/s, the current derived from electric double-layer capacitor can be obtained by the equation (12).

239

$$i_{EDLC}(V) = 0.2 \times k_1 \tag{12}$$

(11)

Where *i*_{EDLC} is the current derived from electric double-layer capacitor. These *i*_{EDLC} points can be linked to form a closed CV curve, which is the shaded part in Figure 3b. The area of shaded part as a percentage of the area of the measured CV curve is the percentage of the contribution of the electric double layer capacitor. The rest is the diffusion-controlled charge contribution. The shadow area is
corresponding to the capacitive current at 0.2 mV/s (Figure 3b), which takes a proportion of 72.7%.
The result demonstrates that capacitive charge contributes 72.7% of the capacity and the diffusioncontrolled charge contributes 27.3% of capacity.

The EIS test for examining the resistance of the as-prepared samples (Figure 3c) shows that each 247 curve has a similar shape which consists of a pressed and rotated semi-circle and a slope line. The 248 pressed and rotated semi-circle is related with the interface resistance between the surface of electrode 249 and the electrolyte bulk. The slope line correlates to the ion diffusion on the surface of electrode.^{45,46} 250 251 It was found that MG-1.6 has relatively small diameter of semicircle, revealing small charge transfer resistance. The result may be attributed to the high conductivity of MG-1.6 arising from the 252 homogenous distribution of MoS₂ particles on the surface of graphene. The slope line correlates with 253 254 the capacitor characteristics and a greater slope of the line means more capacitor characteristics. The inset of Figure 3c shows a relative larger slope line of MG-1.6, suggesting better capacitor 255 characteristics. 256

CDI Performance. Figure 4a shows the Ragone plots of average salt adsorption rate (ASAR_{Na}) 257 versus (vs.) VAC_{Na} of different samples. The result displays that MG-1.6 made the largest decrease of 258 normalized solution conductivity (Figure S8a) and had the largest VAC_{Na} up to 6.0 mg/cm³ and it 259 maintained a high salt adsorption rate even at the high VAC_{Na} stage, which is attributed to the improved 260 microstructure of graphene on MoS₂. Compared to activated carbon, MG-1.6 can save 54% volume at 261 the same adsorption capacity (Table S1). Figure 4b shows the plots of GAC vs. deionization time, and 262 Figure 4c shows the plots of VAC_{Na} vs. deionization time. It is found that GAC_{Na} of MG-1.6 reached 263 to 8.1 mg/g, and still kept a relatively high deionization rate at the high VAC_{Na} stage. The high GAC_{Na} 264

and VAC_{Na} should be attributed to the good ions transfer channel of MG-1.6 resulting from the large 265 fraction of mesopores. GAC_{Na} and deionization rate can be facilitated by favorable pore size 266 distribution. Mesopore is very beneficial to decrease transfer resistance and provides superior ions 267 transfer channel, so that the consumed ions can be replenished quickly from bulk solution, thus very 268 favorable for enhancing deionization capacity. To compared with some reported literatures in the same 269 calculation method, a batch-mode CDI test using the AC || MG-1.6 electrode pairs were carried out 270 (Figure S7a and S7b). The calculation methods of VAC_{NaCl} and GAC_{NaCl} have taken into account the 271 effect of current collectors and both the cathode and anode electrode materials mass. The VAC_{NaCl} and 272 GAC_{NaCl} were calculated to 14.3 mg/cm³ and 19.4 mg/g, respectively. Compared to the reported 273 literatures, the VAC_{NaCl} reaches high level and GAC_{NaCl} is also slightly superior (Figure 4d and S7c, 274 Table 1 and S2).^{25,47-55} The GAC_{Na} and ASAR_{Na} at different flow rates were studied (Figure S8b and 275 276 S8c) and the results show negligible difference among the applied flow rates, implying no obvious impact on GAC_{Na} and ASAR_{Na} and exhibits good stability under different flow rates. Performance of 277 MG-1.6 at different direct voltages was investigated (Figure S9a, S9b and S9c) and a high VAC_{Na} was 278 acquired at 1.2 V. The effect of the initial concentration of NaCl solution on GAC_{Na}, VAC_{Na}, and 279 ASAR_{Na} was studied (Figure S10a, S10b and S10c) and the result shows that both GAC_{Na} and VAC_{Na} 280 increases with the rising initial concentration. The pH value change was investigated during the 281 desalination and regeneration (Figure S11a and S11b). The change of pH may be due to the 282 decomposition of local water.⁵⁶ MG-1.6 also display good performance to remove the heavy metal ions. 283 At low concentration of 0.31 mmol/L Cu²⁺ aqueous solution, the removal rate of Cu²⁺ by MG-1.6 284 reached to 92.3% (Figure S12a). While, at low concentration of 0.48 mmol/L Pb²⁺ aqueous solution, 285 the removal rate of Pb²⁺ by MG-1.6 reached to 91.3% (Figure S12b). A good regeneration ability of 286

MG-1.6 was examined in 100 mg/L NaCl aqueous solution at 1.2 V and 60 mL/min and showed good regeneration stability up to 50 CDI cycles (Figure S13). These results are because of good chemical stability and capacitor characteristics of MG-1.6.

In-situ Raman spectra were conducted for exploring the mechanism of Na-ions storage of MoS₂ (Figure S14). The results show the ratio of characteristic peaks, E^{1}_{2g}/A_{1g} , of 2H MoS₂ decreased with potential decrease from 0 V to -0.5 V at the start stage and increase during the potential increased from -0.5 V to 0.5 V, then decrease during the potential decrease from 0.5 V to 0 V at the end of the whole CV cycle (Figure 5a, Table S3). This result is related with Na⁺ insertion reaction in the interlayers of MoS₂ as follow.

296

$$Na^{+} + xe^{-} + MoS_2 \rightarrow Na_x MoS_2 \tag{13}$$

Because Raman peak A_{1g} is sensitive to interlayer electron density. The binding to electrons during the faradaic reaction (13) lead to increasing the interlayer electron density of MoS₂, resulting in a decrease in A_{1g} strength and an increase in E_{2g}^{1}/A_{1g} .^{57,58}

In order to more clearly prove the phase transformation from 2H MoS₂ to 1T MoS₂, HAADF-STEM 300 was conducted to observe the atom array. A mixed phase in the area was founded indicating the co-301 existence of 2H and 1T MoS₂ after 50 CDI cycles (Figure 5c). Before CDI cycles of the regeneration 302 test, the as-prepared electrode was characterized by Raman spectra and no peaks of 1T MoS₂ was 303 found (Figure 5b). However, after 50 CDI cycles, the characteristic peaks of 1T MoS₂ were found at 304 150 and 233 cm⁻¹ corresponding to the known J1 and J2 peaks.⁵⁹⁻⁶¹ Therefore, an inference that the 2H 305 MoS₂ partly transferred to 1T MoS₂ is reasonable (Figure 5d). For NaCl removal using AC || MG-1.6 306 electrode pairs, the whole deionization process is described below. Firstly, Na⁺ migrates to polarized 307 cathode under electrostatic force and adsorbed on the surface of the electrode. Then, some Na⁺ ions 308

were embedded in the interlayer of MoS₂, and Faradaic reaction (13) occurs and MoS₂ changed from 309 2H phase to 1T phase. Simultaneously, Cl⁻ ions were adsorbed into the electrical double layers between 310 the carbon surface and the bulk NaCl solution. The final material saturates sodium. In the regeneration 311 stage, Na⁺ and Cl⁻ ions adsorbed in the surface electric double-layer are first released. Then, the Na⁺ 312 ions embedded in the MoS₂ layer reacts (14) inversely, and some MoS₂ transforms into 2H phase, 313 while others remain 1T phase. As for the reasons of partial phase transition, more in-depth study is 314 needed. For CDI, we first use HAADF-STEM to study the phase composition in hybrid MoS₂-315 graphene CDI electrodes. The high VAC_{NaCl} electrodes prepared in this study present a promising 316 317 approach to miniaturizing CDI devices for future applications.

318

ASSOCIATED CONTENT

319 **Supporting information**

Non-active materials deionization plots, TEM images, thickness of T_t and T_{cc} , dynamic water contact angle analysis. GCD, CV curves, IR drop and capacitance of different samples. Plots of GAC_{NaCl}, VAC_{NaCl} and NSC *vs*. time for MG-1.6 using AC || MG-1.6 electrode pairs. Plots of NSC *vs*. time for different samples with graphite film as counter electrodes. Plots of NSC, VAC_{Na}, GAC_{Na} *vs*. time for MG-1.6 using GF || MG-1.6 electrode pairs under different condition. Plots of removal of heavy metal ions, NSC and pH *vs*. time, regeneration plots using GF || MG-1.6 electrode pairs. *In-situ* Raman spectra of a CV cycle, comparison of MoS₂-graphene hybrid electrodes and AC electrodes, comparison tables of AC electrode, peaks ratio, reported materials and this work.

327

AUTHOR INFORMATION

328 * E-mail: dszhang@shu.edu.cn.

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501 Figure 1. (a) Schematic illustration of CDI device; (b) Schematic illustration of preparation of MoS₂-graphene

502 hybrids; (c and d) SEM images of MG-1.6; (e and f) TEM images of MG-1.6; (g) HRTEM image of MG-1.6.



505 Figure 2. (a) XRD patterns, (b) N₂ adsorption-desorption isotherms (left) and BJH pore size distribution profiles

Figure 3. (a) GCD curves at a current density of 0.2 A/g (the inset is IR drop of different samples); (b) CV curves at
a scanning rate of 0.2 mV/s (the shadow is the calculated capacitive charge); (c) EIS curves of different samples (the
inset is the full EIS); and (d) Long GCD cycles of MG-1.6 at a current density of 5 A/g.

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Figure 4. (a) Ragone curves of different samples in a 500 mg/L NaCl aqueous solution at 1.2 V and 60 mL/min; (b) Plots of GAC_{Na} *vs.* deionization time of different samples in a 500 mg/L NaCl aqueous solution at 1.2 V and 60 mL/min; (c) Plots of VAC_{Na} *vs.* deionization time of different samples in a 500 mg/L NaCl aqueous solution at 1.2 V and 60 mL/min; (c) Plots of VAC_{Na} *vs.* deionization time of different samples in a 500 mg/L NaCl aqueous solution at 1.2 V and 60 mL/min; (c) Plots of VAC_{Na} *vs.* deionization time of different samples in a 500 mg/L NaCl aqueous solution at 1.2 V and 60 mL/min; (c) Plots of VAC_{Na} *vs.* deionization time of different samples in a 500 mg/L NaCl aqueous solution at 1.2 V and 60 mL/min; and (d) Comparison of VAC_{NaCl} and GAC_{NaCl} between the reported materials and material of this work.

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Figure 5. (a) *In-situ* Raman spectra peak ratio of E^{1}_{2g}/A_{1g} of MG-1.6 during a CV cycle range from -0.5 V to 0.5 V; (b) Raman spectra of MG-1.6 before and after 50 cycles; (c) HAADF-STEM images of MG-1.6 after 50 CDI cycles (the left image corresponding to 1T MoS₂, the right image corresponding to 2H MoS₂); and (d) Schematic illustration of sodiation and desodiation of 2H MoS₂.

Materials	$GAC_{NaCl} (mg/g)$	VAC _{NaCl} (mg/cm ³)	Reference
MoS ₂ -graphene	19.4	14.3	This work
Carbon aerogel	~7	1.43	47
Hollow Carbon sphere	2.3	0.64	48
Mesoporous carbon	14.7	3.56	49
Activated carbon	11	6.26	50
reduced GO/TiO ₂	9.1	4.47	51
TiO ₂ /Carbon	17.4	11.47	52
Carbon nanotube@MnO2	29.77	2.57	53
MnO _x nanofiber	27.8	1.87	54
MoS ₂ /Carbon nanotube	10	18	55
Exfoliated MoS ₂	8.81	16.51	25

 Table 1. Comparison of between reported CDI electrodes and this work.

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