

1 **Transition from oil & gas drilling fluids to geothermal drilling fluids**

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14 **Abstract**

15
16 The harsh downhole conditions encountered in geothermal wells, specifically the high
17 temperatures (HT) together with the toughness of the rock found in many geothermal
18 formations, makes the drilling operation challenging. Drilling in such environments requires
19 specialised drilling fluid formulations that have high thermal stability, good rheological
20 properties, excellent lubricity and low formation damage. Given the wealth of experience in
21 drilling wells in the oil industry, it is tempting to assume that the design of geothermal drilling
22 fluids would be straightforward. However, is this the case? In this literature review, we have
23 attempted to answer the question: “to what degree can developments in oil and gas drilling
24 fluids be transferred to drilling fluids for geothermal wells?” To keep the scope of the review
25 manageable, we have focused on two key aspects of drilling fluid design: rate of penetration
26 (ROP) and HT fluid stability (and maintenance of the desired rheological properties of the fluid
27 at high temperatures). The review has allowed the identification of gaps in both fundamental
28 understanding and in existing technology. Rate of penetration is improved using low viscosity
29 and low-density fluids, and we recommend that foams and aphron systems should be
30 investigated to achieve this (depending on the application pressure). It should be noted,
31 however, that such systems to date have only been studied at relatively low temperatures
32 and the challenge of increasing the thermal stability of the formulation components needs to
33 be addressed. Highly thermally stable polymer systems exist but these are both expensive
34 and not widely available. A systematic study of the impact of copolymer molecular
35 architecture on hydrolytic thermal stability is recommended. A promising solution to both
36 maintaining good rheological properties at high temperature and providing fluid loss control
37 is the use of particulates, especially those in the nano-size range. Additionally, nanocomposite
38 systems show promise in this area and should be investigated. Particle stabilised foams and
39 aphrons are a particularly interesting solution and we recommend that these are studied. It
40 is also recommended to investigate the effect of drilling fluid on long term geothermal well
41 performance.

42 43 **Introduction**

44 The number of geothermal energy exploration and drilling projects designed to access
45 geothermal reservoirs has significantly increased in the last 20 years (De Angelis et al., 2011;

46 Reinsch et al., 2015; Kiran and Salehi, 2020;). One of the major challenges with developing
47 geothermal resources is high drilling costs (Tester et al. 2006; William et al. 2008) Several
48 studies have established that drilling costs can be up to 30% to 70% of the overall project cost
49 (Lowry et al. 2017, Serdjuk, et al. 2013, Finger and Blankenship, 2012). There are many
50 reasons for this. A principal cause is the harsh reservoir conditions encountered in many
51 geothermal well drilling operations. Key challenges include issues related to fluid thermal
52 stability, well control, well integrity, and lost circulation (Chemwotei, 2011; Finger and
53 Blankenship, 2010; Kiran and Salehi, 2020). In addition to high temperatures, hard rock
54 formations impose many technical limitations on selecting drill bits, casing materials, drilling
55 fluids, and cement formulations. These conditions create the need for technological
56 advancements to address HT challenges and rate of penetration issues (Finger and
57 Blankenship, 2010). The HT conditions require the use of specialised drilling fluid formulations
58 which have high thermal stability and can withstand high downhole temperatures, avoiding
59 complications resulting from fluid degradation. The harsh conditions may also damage the
60 casing, cement sheaths, and downhole tools. The most common type of formation rock in
61 geothermal reservoirs are volcanic rocks such as granite, quartzite, granodiorite, and
62 greywacke (Vollmar et al., 2013). These types of rocks are well known for their hardness,
63 which is the resistance of the rock to being scratched, and abrasiveness, which is the ability
64 of the rock to exert wear on metal tools. Both of these factors independently increase the
65 wear on drill bits and shortens their life (Baujard et al., 2017; Finger and Blankenship, 2010;
66 Miyazaki et al., 2019). As demonstrated by Bavadiya et al. (2017), the hardness of the rock is
67 related to drill string vibration, resulting in the failure of downhole tools. Furthermore, the
68 temperature variations in geothermal wells induce thermal stresses on the casing. When
69 these stresses exceed the yield stress of the casing material, the casing fails owing to
70 thermally induced stress fatigue (Shadravan and Amani, 2012; Teodoriu, 2015).

71 Geothermal wells are classified into three categories based on their temperature: low
72 temperature (less than 150°C), medium temperature (between 150 and 200°C), and high
73 temperature (greater than 200°C) (Kruszewski and Wittig, 2018). Furthermore, in some
74 geothermal wells, the temperature can exceed the critical temperature of water, at which
75 point the complexity of drilling and completion operations becomes more challenging (Bland
76 et al., 2006; Kruszewski and Wittig, 2018). The actual temperature that the drilling fluid will
77 be exposed to will be lower than the formation temperature owing to circulation of the mud
78 from surface to the bottomhole and back to the top of the hole (Wang et al, 2023; Kahled,
79 2023). This can reduce the thermal stability requirements of the fluid considerably (by several
80 tens of degrees).

81 The maintenance of drilling fluid properties under downhole conditions, throughout the
82 drilling operation, is crucial. Variations in these properties should be mitigated to ensure
83 efficient and cost-effective drilling (Bland et al., 2006). The elevated temperatures
84 encountered in geothermal wells significantly affect the drilling fluid rheology (Ahmad and
85 Federer, 2018; Fridleifsson et al., 2017). Although bentonite mud is commonly used in
86 geothermal drilling, a substantial increase in the mud yield stress at elevated temperatures
87 has been reported. This increase is attributed to clay swelling and flocculation at high
88 temperatures and sodium ion substitution (Ahmad et al., 2018; Rossi et al., 1999).

89 Additionally, high temperature degrades polymeric additives present in drilling fluids and
90 lowers the viscosity of the drilling fluid thus reducing its performance (Amani, 2012;
91 Chemwotei, 2011; Kruszewski and Wittig, 2018; Lee et al., 2011; Sukhoboka, 2017; Tehrani et
92 al., 2007). It was reported that high-pressure increases the viscosity and yield point of oil-
93 based drilling muds by changing the volume of continuous phase owing to compression
94 (Amani and Al-Jubouri, 2012a; Rossi et al., 1999). However, the impact of change in pressure
95 on fluid properties such a viscosity is less than the effect of changes in temperature (this is
96 intrinsic to the Clapeyron equation which describes the relationship of change in pressure and
97 temperature on material properties) (Amani and Al-Jubouri, 2012b; Bybee, 1999; Davison et
98 al., 1999; Sukhoboka, 2017).

99 In principle, the drilling operations of geothermal and oil and gas wells are similar (Bavadiya
100 et al., 2019; Capuano, 2016; Saleh et al, 2020). However, in reality high temperature and
101 pressure wells in the oil and gas industry are a niche market, which has led to a reduced
102 research and development effort. To unlock geothermal energy with a focus on achieving net
103 zero, a systematic study is required to understand the technical and scientific gaps in our
104 knowledge and to identify any transferrable learnings from oil and gas drilling. This is
105 especially true of drilling fluids used for drilling in high temperature environments. However,
106 to date there has been no systematic study of the properties and behaviour of drilling fluids
107 developed for high temperature (HT) oil and gas drilling operations compared with the
108 technical requirements for geothermal drilling fluids. In this paper we attempt to address this
109 gap by reviewing the literature to understand the requirements of a geothermal drilling fluid
110 and compare these to the properties and behaviour of oil and gas drilling fluids. This has
111 allowed us to identify the gaps in both fundamental understanding, in the existing technology
112 and to elucidate the key technical challenges that remain.

113 Our analysis of the literature identified three main problems in geothermal drilling operation:
114 1. Poor rate of penetration; 2. Maintenance of optimal rheology at high temperatures
115 (essentially maintaining a highly shear thinning fluid with sufficient low shear gel strength);
116 and 3. The lack of fluids offering thermal stability beyond *ca.* 260 °C. Accordingly, the
117 following review is divided into three main sections discussing rate of penetration and the
118 impact of drilling fluid properties on this, polymer hydrolytic thermal stability, and the impact
119 of solid stabilisers on fluid thermal stability. In the rate of penetration section, we identify
120 solutions to this problem and suggest some research avenues. The polymer section discusses
121 biopolymers separately to synthetic polymers and focuses on the properties that each
122 monomer imparts to the final polymer attempting to identify the effect of the functional
123 groups of the monomers on fluid thermal stability. We have attempted to identify and discuss
124 studies that either have suitable laboratory data, or, ideally, field data illustrating the effect
125 of the polymer on the thermal stability of the formulated fluid. The final section discusses the
126 effect of solids as viscosifiers and fluid stabilisers. Since this is the more under-researched
127 area, we identify gaps in knowledge and suggest avenues of research to improve our
128 understanding of these materials.

129 **Literature Review**

130 **Factors affecting rate of penetration (ROP)**

131 The key questions that we tried to answer were:

- 132 1. What are the key parameters governing ROP?
- 133 2. Does ROP depend on rheology / composition of drilling fluid?
- 134 3. Can we make recommendations for new drilling fluid formulations to enhance ROP?

135 The area has been recently extensively reviewed by Najjarpour *et al* (2021, 2022a, 2022b).
136 Historically, ROP management has mainly focused on analytical and semi-analytical models
137 with several correlations being developed for this purpose. The key conclusions that can be
138 derived based on the work of Najjarpour *et al* are:

139 1. The Bourgoyne and Young (1974) (B&Y) regression model is the most commonly employed
140 model for ROP management, whilst that of Hareland and Hoberock (1993) is the second most
141 used.

142 2. The B&Y equation, or a modified version thereof, is suggested by Najjarpour *et al* as the
143 best choice when an analytical or semi-analytical model is required for ROP management.

144 3. ROP depends on the rheology / composition of the drilling fluid.

145 4. ROP increases linearly with decreasing plastic viscosity, solid content, and mud weight for
146 both sedimentary and geothermal rock formations.

147 5. Artificial intelligence algorithms have been used in many ROP management studies This is
148 because the prediction accuracy, in most cases, is good and the computing cost is low.

149 6. Several different machine learning (ML) approaches have been tried for ROP management
150 with varying degrees of success. Many of the ML models are based on the B&Y model, but
151 they do not include detailed drilling fluid properties – non-Newtonian rheology at HT,
152 filtration (filtercake thickness / permeability), formation damage, etc. Promising machine
153 learning approaches to rheological property prediction that could be coupled to ROP
154 prediction are described by Davoodi *et al.* (2023c).

155 A key learning from the ROP literature is that ROP is increased when fluid viscosity and mud
156 weight (essentially density) is decreased. However, in practice, a low viscosity might not be
157 optimal at all times because for such factors as hole cleaning / avoiding cuttings
158 sedimentation at low shear rate (or in quiescent state), a high viscosity is desirable (Caenn *et*
159 *al.*, 2017). Therefore, ideally a shear-thinning fluid is required. We discuss the consequences
160 of this later in the paper.

161 **High Temperature Tolerant Fluids for Oil and Gas drilling**

162 High temperatures are a challenge in oil and gas drilling owing to the degradation of fluid
163 properties, greatly reducing the ability to drill at high rate (Agwu *et al*, 2021; Gautam *et al*,
164 2022). In particular, the rheology of the fluid is significantly impacted under HT conditions.
165 The cause of this is a combination of bentonite flocculation and the degradation of polymeric
166 viscosifying agents (Kelessidis, 2009; Ali *et al*, 2020; Gautam *et al*, 2022). It is therefore
167 challenging to maintain the desired equivalent circulation density (ECD) and viscosity since
168 these both decrease as temperature increases. This impacts ROP and introduces considerable

169 risk to the safety of the drilling operation (Maghrabi et al., 2011; Rommetveit and Bjorkevoll,
 170 1997; Wang et al., 2012a).

171 **HPHT additives: structure-property relationships**

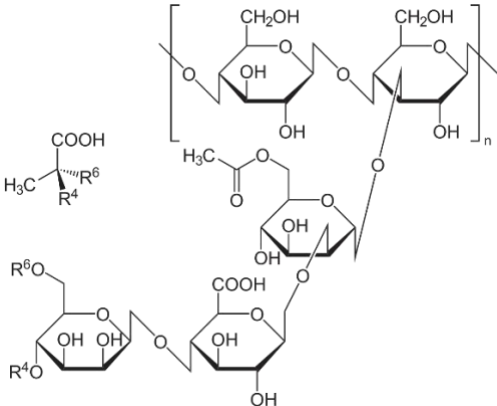
172 Various varieties of natural polymers, synthetic polymers, nanoparticles, and minerals have
 173 been frequently used as additives for drilling fluids. The performance of these additives
 174 depends on their structure and functional and physical properties. In general, these additives
 175 improve thermal properties of drilling fluids by acting as dispersants for bentonite preventing
 176 flocculation and by maintaining structural integrity at high temperature, thus maintaining the
 177 rheological properties of the fluid (Gautam et al, 2022).

178 **Polymeric Additives**

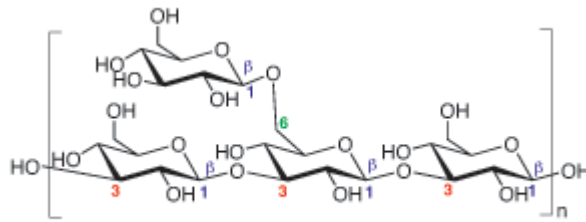
179 Polymers (natural and/or synthetic) are a common additive for HT fluid formulation in oil
 180 and gas drilling operations. The following sections discuss the range of polymers that have
 181 been tested and deployed.

182 **Biopolymers**

183 Table 1 lists organic polymers that have been used in water-based drilling fluid formulations
 184 and lists the properties that the polymer imparts to the fluid.

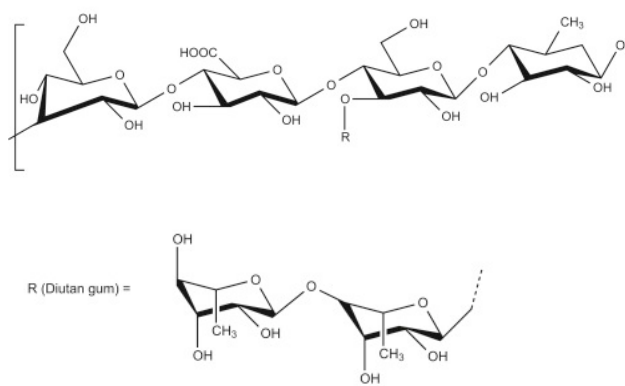
Polymer	Structure	Properties imparted
Xanthan gum		<p>Xanthan gum is a natural water-soluble high molecular weight polysaccharide produced by a fermentation process. Owing to its exceptional rheological properties (it adopts a double-helical conformation which leads to a shear thinning rheological profile), it is a very effective viscosifying agent for water-based drilling fluids (Caenn et al, 2017). It is environmentally benign (used as a food additive) but is temperature sensitive and loses its ability to viscosify fluids beyond 90 °C (Lambert et al, 1985).</p>

Scleroglucan

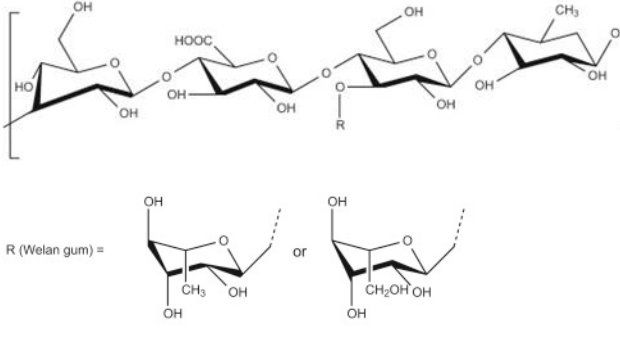
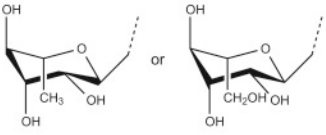
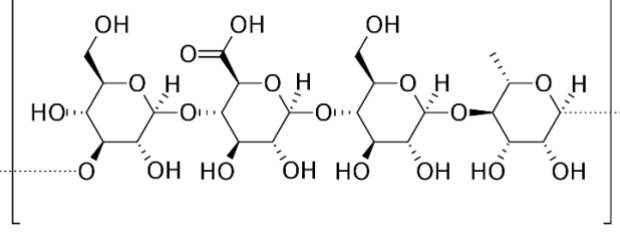


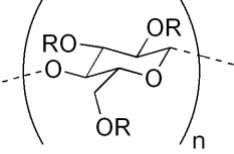
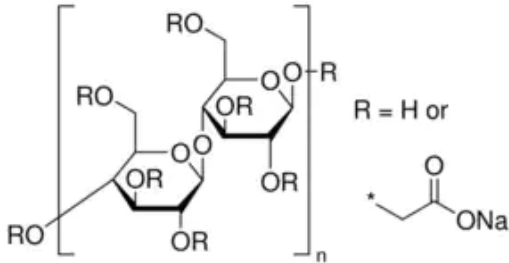
Scleroglucan (also known as schizophyllan) is an extracellular polymeric substance of glucose produced by fungi. It is a high molecular weight, non-ionic polysaccharide composed of a (1,3)-β-d-glucopyranosyl backbone with (1,6)-β-d-glucopyranosyl residues as branches. It has better shear, salinity (non-ionic material) and thermal degradation resistance than xanthan gum. Its viscosifying behaviour is similar to xanthan and it is also environmentally benign (Kalpakci et al, 1990).

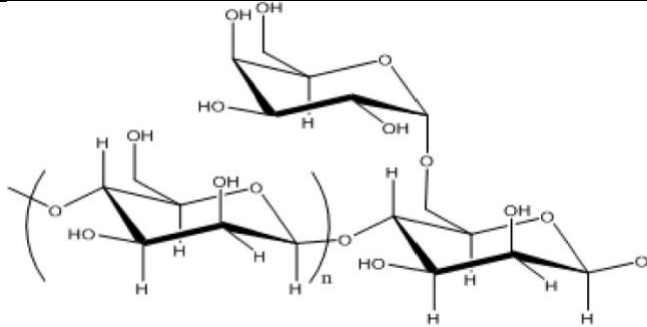
Diutan Gum



Diutan gum is a natural high-molecular-weight gum produced by carefully controlled aerobic fermentation. The repeating unit is composed of a six-sugar unit. The backbone is made up of d-glucose, d-glucuronic acid, d-glucose, and l-rhamnose, and the side chain of two l-rhamnose. It adopts a double-helical conformation where the side chains screen the carboxylate groups of the backbone and prevent cross-linking by calcium ions. The rheological profile is shear thinning and it is more thermally

		stable than xanthan gum (Mota and Pereira, 2022)
Whelan Gum	 <p>R (Welan gum) = </p>	<p>Whelan gum is like Diutan gum, except that the side chains contain a single unit of either L-mannose or L-rhamnose. In aqueous solution, it adopts a double-helical conformation where the side chains screen the carboxylate groups of the backbone and prevent cross-linking by calcium ions. The rheological profile is shear thinning. It is stable above 90 °C (Benning et al, 2016; https://www.oceanviewchem.com/welan-gum.html)</p>
Gellan Gum		<p>Gellan gum is a water-soluble anionic polysaccharide produced by the bacterium <i>Sphingomonas elodea</i>. The repeating unit of the polymer is a tetrasaccharide, which consists of two residues of D-glucose and one of each residue of L-rhamnose and D-glucuronic acid. It exhibits a sol-gel transition in which there is a conformation change from random coil to double helix during cooling followed by aggregation of the double helices. The sol-gel transition temperature and gel strength of gellan gum depend on the cation</p>

		<p>species, polymer, and cation concentration. Compared to monovalent cations (K^+ and Na^+), divalent cations (Mg^{2+} and Ca^{2+}) can promote a more efficient gelation which is advantageous in a drilling fluid. The thermal behaviour is inferior to xanthan gum (Goa, 2015)</p>
<p>Hydroxyethyl cellulose (HEC)</p>	 <p>R = H or CH_2CH_2OH</p>	<p>Hydroxyethyl cellulose (HEC) polymer is a hydroxyethyl ether of cellulose, obtained by treating cellulose with sodium hydroxide and reacting with ethylene oxide. The polymer shows strong viscoelastic behaviour in aqueous solution (Ouaer and Mourad, 2018).</p>
<p>Sodium Carboxymethyl cellulose (CMC)</p>	 <p>R = H or</p>	<p>Carboxymethyl cellulose (CMC) or cellulose gum is a cellulose derivative with carboxymethyl groups ($-CH_2-COOH$) bound to some of the hydroxyl groups of the glucopyranose monomers that make up the cellulose backbone (Caenn et al, 2017).</p>

<p>Guar Gum</p>		<p>Guar gum is a natural non-ionic polymer obtained from the annual agricultural crop <i>Cyamopsis tetragonolobus</i>, belonging to family leguminosae. Guar gum has been utilized as emulsifier, thickener, and stabilizer in the food and beverage industry and pharmaceutical chemicals in the pharmaceutical and cosmetics industry for a long time (Sharma et al, 2018). Nowadays, the petroleum industry is the biggest consumer of Guar gum and more than 40% of the world's Guar is used as additives in hydrofracking fluid (Hasan, A.M. and Abdel-Raouf. 2018)</p>
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186 **Table 1. Organic (bio)polymers used in water-based drilling fluid formulations.**

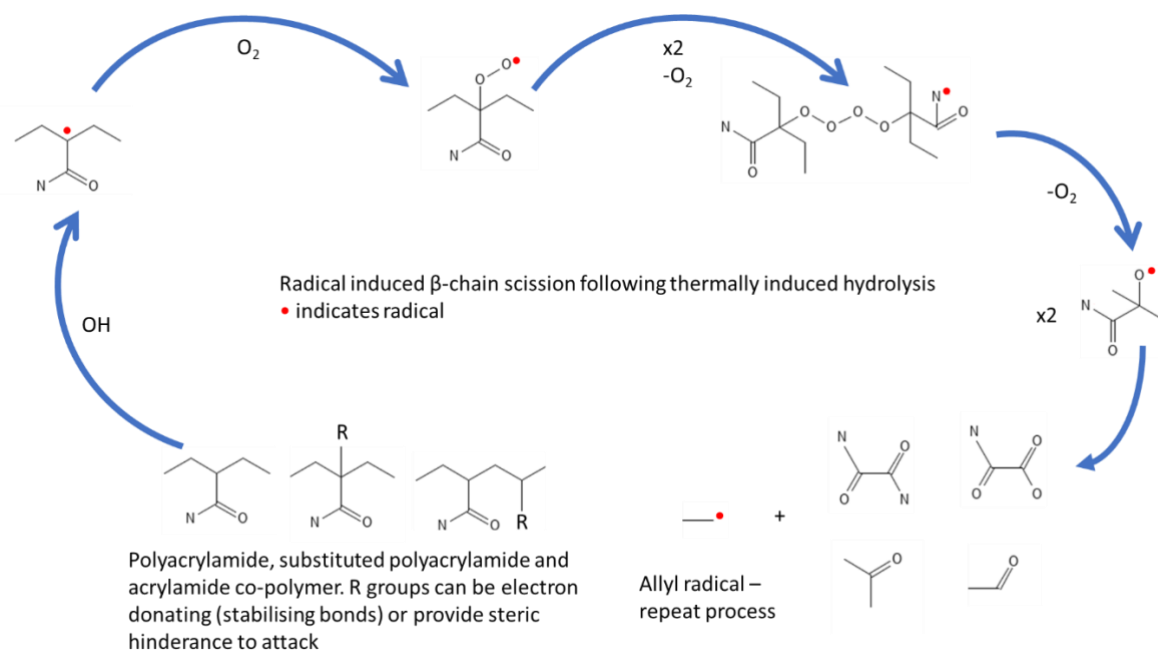
187 Unmodified natural polymers are not stable at the ultra-high temperatures often found in
 188 geothermal energy drilling operations (>200 °C) because of the low hydrolytic stability of the
 189 carbon-oxygen bond (acetal bond) found in the backbone of all of these polymers. Whilst the
 190 intrinsic bond strength of a paraffinic C-O is greater than a C-C bond, the high
 191 electronegativity of the oxygen atom makes the bond susceptible to nucleophilic and free
 192 radical attack with an OH leaving group. This is demonstrated by the low thermal stability of
 193 xanthan gum in aqueous solution (90 -120°C; Lambert et al, 1985, Xie and Lecourtier, 1992).
 194 Of the natural polymers employed in drilling fluids, scleroglucan displays the highest thermal
 195 stability with an effective high stability of 135 °C (Kalpakci et al, 1990).

196 The thermal stability of natural polymers can be increased by functionalising them, by grafting
 197 them to synthetic polymers, and by forming polymer-inorganic composites. This is discussed
 198 later in this review. Additionally, the use of oxygen scavengers to reduce the concentration
 199 of oxygen to prevent corrosion helps with polymer stability under downhole conditions
 200 (Audibert and Lercoutier, 1993). This is because of the reduction in the concentration of free
 201 radicals of oxygen that attack the polymer backbone. This method is also effective for

202 synthetic polymers (Zheng et al, 2020). The most common scavenging agents are erythorbic
 203 acid, sodium sulfite, and ammonium bisulfite (MacMohan et al, 2002).

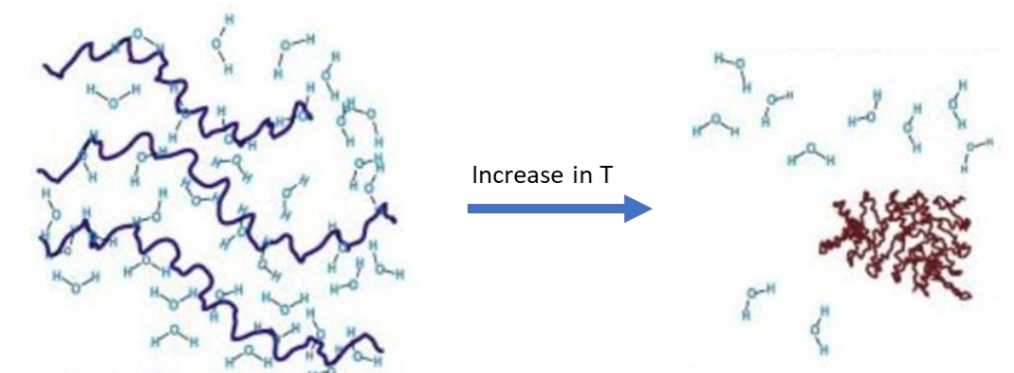
204 **Synthetic Polymers**

205 The hydrolytic thermal stability of polymers is complicated and not without controversy
 206 (Vijayalakshmi and Madras, 2006; Oliveira *et al*, 2019). However, free radical attack at the
 207 backbone of polymers such as polyacrylamide in the presence of oxygen is a known pathway
 208 leading to chain scission and most probably the main route to degradation (Ma *et al*, 2015;
 209 Xiong *et al*, 2019; Vohlídal, 2020). This is illustrated in Figure 1 below.



210
 211 **Figure 1. The Free Radical Route to Chain Scission in Polyacrylamide. In this Figure ^ denotes**
 212 **a radical.**

213 In addition to polymer degradation, high temperature promotes polymer chain conformation
 214 changes that result in a loss of viscosity. At low temperatures the polymer chains are well
 215 hydrated and extended in solution allowing them to entangle and impart a high viscosity. As
 216 the temperature is increased, the chains can start to lose waters of hydration (that is the
 217 solvency of the water is reduced) causing the polymer to collapse and 'ball up' thus resulting
 218 in a loss of viscosity (De Gennes, 1979). This is illustrated in Figure 2 below.

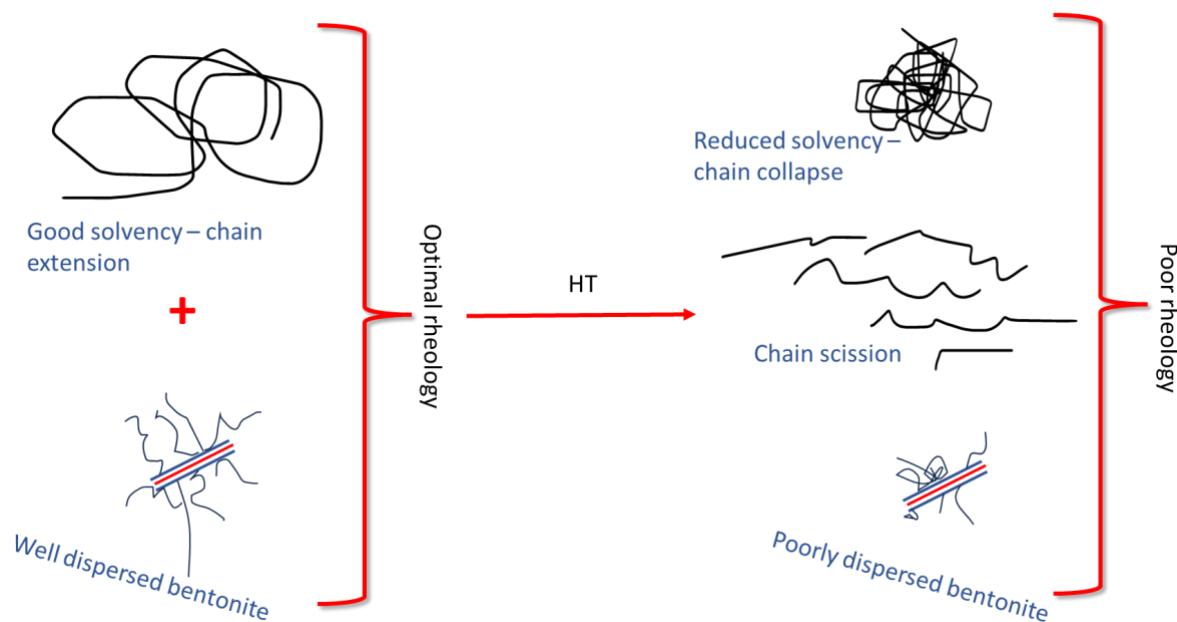


220 **Figure 2. Cartoon illustrating the change in polymer chain conformation with increasing**
221 **solution temperature.**

222 This effect can be reduced by introducing co-monomers that protect hydrophilic groups or by
223 imparting steric resistance to conformation changes (Gautam *et al.*, 2022; Davoodi *et al.*, 2023).

224 Finally, high temperatures can induce hydrolysis of the pendant amide groups in acrylamide-
225 based polymers which produces carboxyl groups (Ma *et al.*, 2015). This can lead to
226 precipitation of the polymer in saline waters through chelation with calcium ions and by
227 crosslinking via cation bridges with a consequent reduction in viscosity and yield point.

228 These polymeric changes (degradations) have an impact on fluid rheology both directly and
229 indirectly by a reduction in the ability of the polymer to disperse bentonite (particles through
230 changes in adsorption capacity, changes in polymeric charge, and by chain length reduction).
231 These effects all have impacts on key parameters such as ROP and the hole cleaning ability of
232 the fluid. Figure 3 provides a visual summary of these effects.

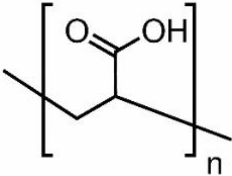
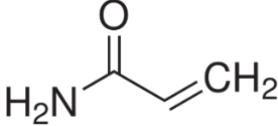
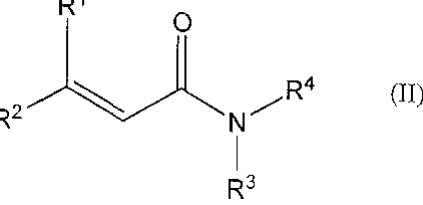


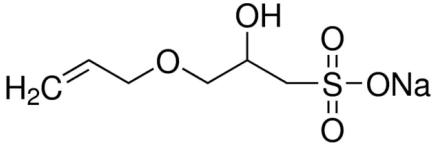
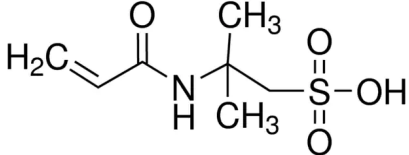
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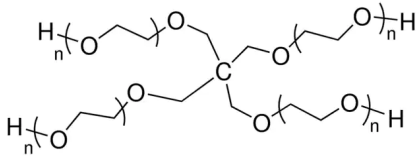
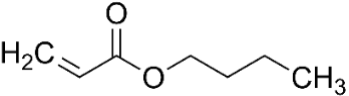
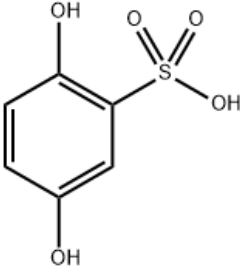
234 **Figure 3. A summary of the impact of high temperatures on drilling fluid rheology**

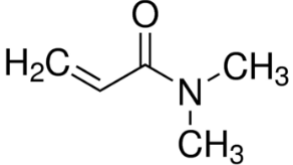
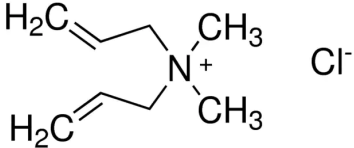
235 Table 2 lists the monomers that have been employed to make polymeric additives for drilling
236 fluid use. The table lists the key properties imparted by the monomer to the polymer physical
237 properties.

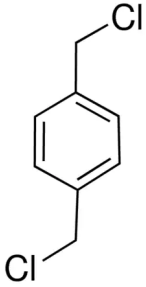
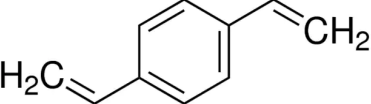
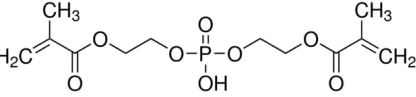
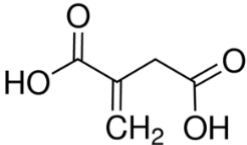
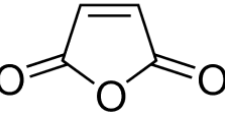
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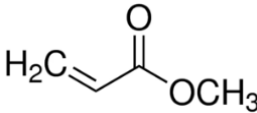
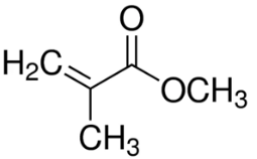
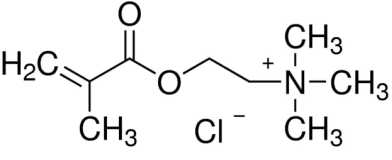
Polymeric monomer	Structure	Properties imparted
Acrylic acid (AA)		<p>The carboxyl group provides a high degree of hydrophilicity to polymers containing this monomer and helps to maintain clay dispersion by forming intermolecular hydrogen bonds with clay platelets (Somiya, 2013).</p> <p>Furthermore, the high charge density imparted by the carboxyl group “shields” the polymers in high salt concentration brines preventing precipitation and loss of viscosity; it also improves stability in acidic pH (Sennakesavan et al., 2020).</p>
Acrylamide (AM)		<p>Acrylamide forms the basis of most water-soluble polymers used in industry. It is relatively cheap monomer and is highly reactive so simple to polymerise. In polymers, the acrylamide monomer displays improved dispersion of clays and acts as a viscosifying agent (Caenn et al, 2017)</p>
Alkyl-substituted acrylamide (AAM)		<p>The amide group present in the monomer contributes to hydrophilicity of polymers containing this monomer and offers a site for hydrogen bonding, whereas the alkyl functional groups provide resistance towards</p>

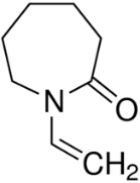
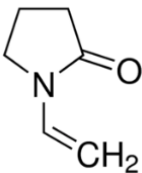
		alkaline hydrolysis of the polymer (Perricone et al., 1986)
3-(allyloxy)-2-hydroxy-1-propane sulfonic acid (AHPS)		The hydrophilic sulfonic acid group provides hydrolytic (and hence thermal) stability to polymers containing this monomer in high salt concentration brines (Sepehri et al., 2018)
2-acrylamido-2-methyl-1-propane sulfonic acid (AMPS)		<p>The combined effect of geminal dimethyl and sulfo-methyl group sterically hinders the reactivity of the non-ionic amide group (-CONH-) and imparts resistance of polymers containing this monomer to chemical decomposition (i.e., hydrolytic stability that enhances dispersibility and thermal stability).</p> <p>Furthermore, AMPS exhibits a high degree of hydrophilicity and anionic character at a wide range of pH, which is mainly owing to the presence of the sulfonic acid group in AMPS, and results in the enhanced water absorbing capacity with a high degree of water solubility (Jiang et al., 2019; Meng and Ye, 2017).</p> <p>Moreover, the sulfonic acid group in AMPS completely ionizes in aqueous solutions with a high ionization constant (Meng and Ye, 2017). As a result, it inhibits the precipitation</p>

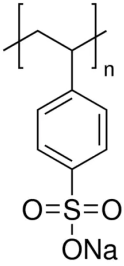
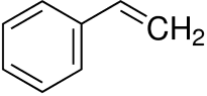
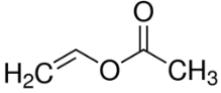
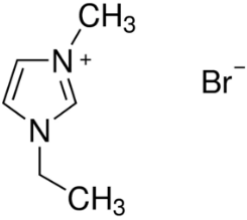
		<p>of numerous cations, including calcium and magnesium,</p> <p>(Liu et al., 2003; Rivas et al., 2001).</p> <p>Therefore, AMPS containing polymers are the ideal additive for drilling fluids designed to be used in high salinity and/or HPHT conditions (Plank, 1992).</p>
Allyl-polyoxyethylene ether (APEG)		<p>The hydrophilic polyoxyethylene chains are reported to protrude in the aqueous phase and thus, impart steric repulsion and help control colloidal aggregation at high temperature and salinity (Liu et al., 2018).</p>
Butyl acrylate (BA)		<p>The vinyl and butyl-linked carboxylate ester groups in the monomer provides hydrophobic character to the associated copolymers and aids in thermal stability (Al-Muntasheri et al, 2008)</p>
potassium 2,5-dihydroxy benzene sulfonate (DHBS)	 <p style="text-align: center;">KH</p>	<p>The aromatic phenyl group provides rigidity to the copolymer, thus improving the thermal stability. The hydrophilic sulfonate group enhances the dispersion of bentonite by reducing the attraction between bentonite particles by electrostatic stabilization and plugging the filter cake holes (Peng et al., 2010)</p>

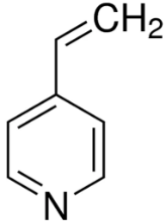
<p>N, N' dimethyl acrylamide (DMAM)</p>		<p>The unshared electron pair on the monomer promotes adsorption on clay surfaces. Furthermore, the non-polar dimethyl group promotes hydrolytic (and hence thermal) stability in polymers containing the monomer (Nagre et al., 2016)</p>
<p>dimethyl diallyl ammonium chloride (DMDAAC)</p>		<p>The dimethyl group in the monomer provides steric hindrance to the cationic quaternary ammonium moiety (Wang et al., 2011b) and promotes hydrolytic (and hence thermal) stability of polymers containing the monomer.</p> <p>In addition, the DMDAAC monomer undergoes cyclic-polymerization leading to the formation of a new five-member ring pyrrolidine structure, improving the thermal stability of DMDAAC-containing polymers (Jia et al., 2019).</p> <p>The cationic charged quaternary ammonium moiety is absorbed by negatively charged clays (such as bentonite). The bond formed between quaternary ammonium and bentonite is stronger than the intermolecular hydrogen bonds, thereby enhancing the thermal stability of the drilling fluid (Lin and Luo, 2015).</p>

<p>α,α' -dichloro-p-xylene (DPX)</p>		<p>The phenol groups provide rigidity to the polymer which improves thermal stability (Zhang et al, 2018)</p>
<p>p-divinyl benzene (DVB)</p>		<p>The rigidity of the phenyl group enhances thermal stability of polymers containing the monomer. Furthermore, the monomer can cross-link directly to other polymer chains, improving the thickening properties of the polymer (Xie et al., 2016)</p>
<p>Bis(hydroxyethyl methacrylate phosphate) (HEMA)</p>		<p>The pendant hydroxyl group imparts hydrophilic characteristics to associated copolymers and swells in water (Nagre et al., 2021)</p>
<p>itaconic acid (IA)</p>		<p>The two carboxyl functional groups present in the monomer give associated polymers a high degree of hydrophilicity) and aid the polymer at high salt concentrations under HPHT conditions (Teleky and Vodnar, 2019.</p>
<p>Maleic Anhydride (MA)</p>		<p>Maleic anhydride is an acid anhydride of maleic acid and exhibits hydrophilicity and highly anionic characteristics owing to the</p>

		presence of two carboxyl groups. In addition, the heterocyclic furan improves the thermal stability of polymers containing the monomer (Lalehgani et al., 2019).
Methyl acrylate (Mac)		The carboxylate ester group in the monomer impart hydrophilic character to associated copolymers and aids in hydrolytic stability and dispersion. The pendant methyl group sterically shields the ester linkage and improves salt tolerance (Ali et al, 2015)
Methylmethacrylate (MMA)		The pendant methyl group in the monomer sterically shields the ester linkage from chemical attack (improves salt and calcium resistance) (Dodiuk, 2013) in associated polymers.
2-(methacryloyloxy)ethyl]trimethylammonium chloride (METAC)		The positively charged N+(CH3)3 group is strongly adsorbed onto the surfaces of clays and prevents the flocculation of clay particles. This helps in controlling the rheological and filtration characteristics of drilling fluids at HT conditions. In addition, the end methyl group imparts thermal and hydrolytic stability to the associated polymer (Xiping et al., 2016)

<p>N-vinyl caprolactam (NVCL)</p>		<p>Polymers containing NVCL exhibit a lower critical solution temperature - at this temperature, the polymer undergoes a reversible phase transformation from the coil to the globule conformation (Kozlovskaya and Kharlampieva, 2019). In addition, the copolymers of NVCL undergo a ring-opening reaction when exposed to high temperatures resulting in the formation of a secondary amine structure on the backbone of the polymer. This leads to a greater molecular volume of polymer in aqueous solutions and increases the solution viscosity (Thaemlitz, 2006).</p>
<p>N-vinyl pyrrolidone (NVP)</p>		<p>The inelastic lactam group provides thermal stability to the polymer, and the vinyl group offers nucleophilic reactions with active-hydrogen-bearing functional groups. The amide carbonyl group is nucleophilic at the oxygen site, and this property enables the formation of intermolecular hydrogen bonds which improve dispersibility of clays. The presence of both hydrophilic and hydrophobic functional groups enhances the solubility of the polymer (Haaf et al., 1985).</p>

<p>sodium 4-styrene sulfonate (SSS)</p>	 <p>The structure shows a polymer backbone with a styrene unit (vinyl group attached to a benzene ring) and a sulfonate group (-SO₃Na) attached to the para position of the benzene ring.</p>	<p>The benzene sulfonate group imparts salt-resistant and high temperature stability to associated polymers and aids in clay dispersion. Furthermore, the aromatic benzene ring provides hydrophobic characteristics to the monomer and thus additionally improves the thermal stability of the associated polymer (Liu et al., 2020)</p>
<p>Styrene (ST)</p>	 <p>The structure shows a benzene ring attached to a vinyl group (-CH=CH₂).</p>	<p>The aromatic benzene ring provides hydrophobic characteristics to the monomer and thus improves the thermal stability of the associated polymer (Liu et al., 2020)</p>
<p>Vinyl acetate (VA)</p>	 <p>The structure shows a vinyl group (H₂C=CH-) attached to an acetate group (-O-C(=O)-CH₃).</p>	<p>The acetate group provides a high degree of hydrophobicity and thus, helps improve the thermal stability of VA-copolymers (Nagreg et al, 2016)</p>
<p>1-vinyl-3-ethyl imidazolium bromide (VEIBr)</p>	 <p>The structure shows an imidazolium ring with a methyl group on one nitrogen and a vinyl group on the other. The counterion is a bromide ion (Br⁻).</p>	<p>The imidazole structure exists in tautomeric form, and hydrogen can bond to any nitrogen atoms, making it highly polar with the electric dipole moment of 3.67 D. The rigid hetero-aromatic imidazole structure improves the thermal stability of associated polymers. The cationic quaternary ammonium group improves calcium resistance by adsorption onto bentonite platelets (Christen et al, 1981).</p>

<p>4-vinyl pyridine (VP)</p>		<p>The nitrogen centre of pyridine features a lone pair electron and thus, makes chemical properties like that of tertiary amines.</p> <p>Interestingly, the pyridine ring undergoes protonation to form a conjugate acid with an acid dissociation constant of 5.25 This behaviour helps control colloidal stability and filtration loss while drilling in high calcium (Ca^{2+}) concentrations and under acidic pH conditions (Pal, 2018).</p>
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240 **Table 2. Monomers used to form homo and co-polymers used as drilling fluid additives in water-based fluids.**

241 Two recent reviews have surveyed the use of synthetic polymers as drilling fluid additives (Davoodi et al, 2023a, 2023b) covering all functional
 242 aspect of the polymer in drilling fluids. Here we focus principally on the rheological properties of the fluid at high temperatures and specifically
 243 focus on the impact of different monomers and combinations of monomers on the thermal stability of the polymer.

244

245 ***Homopolymers***

246 A homopolymer is a chain of chemically linked with identical monomer units. These polymers
247 exist as flexible coils and are relatively easy to prepare and contain evenly distributed
248 functionality throughout their backbone (Moerdyk and Bielawski, 2012).

249 Most industrial water-soluble polymers are based on acrylamide and acrylic acid polymers.
250 These homo-polymers are then functionalised to improve or add performance to the
251 polymer.

252 ***Polyacrylamide (AM)***

253 Polyacrylamide is a water-soluble polymer formed by the polymerization of either acrylamide
254 monomers or N,N'-methylenebis(acrylamide). In practice, the thermal limit for
255 polyacrylamide containing drilling fluids appears to be up 150 °C (Alireza and Majid, 2013),
256 although others have found a practical limit of ca. 90 °C (Borthaker et al, 1997) and can be
257 lower in brines containing high concentrations of divalent ions (Omer, 2012). Silva et al. (2000)
258 studied the thermal stability of polyacrylamide using thermo-gravimetric analysis (TGA) and
259 reported that the thermal stability of polyacrylamide might be due to the presence of the
260 hydrogen bonds present within the matrix. This also reduces the mobility of the polymer chain
261 and therefore, increases the thermal strength. There is, however, a large disparity between
262 the TGA thermal stability (300°C) and the practical field-based stability (~90°C). This is
263 because the brine that dissolves the polymer acts to reduce the effectiveness of the polymer
264 at providing viscosity to the fluid and controlling fluid loss.

265 ***Polyvinyl pyrrolidone (PVP)***

266 Tehrani *et al.* (2007) developed a WBM system comprising of polyvinyl pyrrolidone (MW: 360,
267 000 Da), shale inhibitor (polyoxy-alkylene glycol), dispersant (Zirconium citrate), and weighing
268 agent (Manganese tetroxide). The primary role of the polyvinyl pyrrolidone is as a high
269 temperature deflocculant, owing to the nucleophilic amide carbonyl group that forms
270 intermolecular hydrogen bonds. In contrast, the inelastic pyrrolidone functional group
271 improves thermal stability. The formulation was found to be stable up to 356 °F (180 °C)) and
272 relies on the synergism between weighing material and polymers to achieve stable and
273 controllable rheological properties.

274 ***Poly(sodium 4-styrene sulfonate) (SSS)***

275 Liu *et al.* (2020) studied the effect of poly sodium 4-styrene sulfonate (PSS) on the thermal
276 stability of formulated WBMs. Poly(sodium 4-styrene sulfonate) is a homopolymer of sodium
277 styrene sulphonate (SSS). It was observed that, with 1.0 wt% addition of PSS, the water-based
278 drilling fluid remained stable at a temperature of 392 °F (200 °C). The PSS significantly reduced
279 the aggregation of bentonite particles; this is attributed to the presence of a highly anionic
280 sulfonate functional group that adsorbs onto the bentonite clay particles. In addition, PSS
281 limits the coarsening of particles, resulting in stable rheology. The drilling fluid cake thickness
282 and cake permeability were lower than those of drilling fluid without PSS, leading to effective

283 control of filtration. Finally, the PSS-based fluid was used to drill an HPHT deep well in Xinjiang
284 province, China, with a bottom hole temperature of 328 °F (165 °C).

285 ***Copolymers***

286 A copolymer is a class of polymer formed when two or more different types of monomers are
287 linked in the same polymeric chain. The goal of incorporating two or more monomers into a
288 single polymer chain is to generate desirable physical and chemical properties that are not
289 available with homopolymers (Scott and Penlidis, 2017). The macroscopic behaviour of a
290 copolymer is significantly affected by the sequence and chain architecture of the
291 comonomers. In addition to this, a copolymer may exhibit microstructural variations such as
292 stereochemical isomerism and regioisomerism. Based on the chain architecture, a copolymer
293 can be classified into linear, branched, crosslinked, and graft copolymers.

294 ***Linear copolymers***

295 ***Styrene sulfonic acid-maleic anhydride (SSMA) copolymer***

296 Chesser and Enright (1980) synthesized a low molecular weight copolymer (MW: 1000–5000
297 Da) involving sulfonated styrene and maleic anhydride. The functional groups (sulfonate) in
298 the SSMA copolymer provide a high charge density which promotes adsorption on clay edges
299 at elevated temperatures leading the clay particles remaining dispersed (preventing
300 flocculation). In addition, the five-membered heterocyclic furan ring in maleic anhydride and
301 the benzene ring of the SSS monomer improve the thermal stability of the copolymer. It is
302 reported that the thermal decomposition of the copolymer was determined using thermos
303 gravimetric analysis (TGA) and was found to be higher than 752 ° F (400 °C) (Chesser and
304 Enright, 1980). The molecular arrangement of monomers in the copolymer favours steric
305 hindrance, leading to stronger hydrogen bonding compared to higher molecular weight
306 deflocculants (Chesser and Enright, 1980). The performance of SSMA polymer was evaluated
307 in both the laboratory and the field. No fluid thickening was observed up to 500 ° F (260 °C),
308 indicating the effectiveness of the additive as a high temperature deflocculant. In addition,
309 the deflocculated state of the fluid at high temperatures improved the filtration performance.
310 Although the SSMA performed satisfactorily in freshwater, the high electrolyte concentration
311 of the seawater employed offshore had a detrimental effect on performance (Hille, 1985).

312 Audibert *et al.* (1999) reported the development of a novel polymeric filtration control
313 additive comprising styrene sulfonate monomer. The polymer components were screened to
314 optimize thermal stability, minimize rheological impact and limitations arising from formation
315 damage due to fluid invasion. The developed additive was tested in a freshwater-based fluid,
316 and no gelation of bentonite was observed after aging at 320 ° F (160 °C).

317 ***Vinyl sulfonate and vinyl amide (VSVA) copolymer***

318 Lucas *et al.* (1981) developed a copolymer comprising of vinyl sulfonate (AMPS) and vinyl
319 amide monomers, made using a solution polymerization technique. The copolymer enhances
320 the formation of an impermeable filter cake after exposure to high temperatures,
321 predominantly owing to the adsorption of polymer molecules onto clay particles; this hinders

322 the penetration of water through the filter cake, effectively reducing filtration losses.
323 Furthermore, owing to the presence of the sulfonate moiety, the copolymer offers enhanced
324 salt tolerance. Son *et al.* (1987) investigated the thermal stability and electrolyte resistance
325 of filtration control additives such as polyacrylate (PA), partially hydrolysed poly acrylamide
326 (PHPA), and VSVA copolymer. It was observed that the vinyl backbone improves the thermal
327 stability of the PA and PHPA copolymers. However, at a high pH value, the acrylamide group
328 undergoes alkaline hydrolysis (Fieser and Fieser, 1961). Incorporating sulfonate groups in the
329 polymer (VSVA copolymer) gives the polymer chains a high charge density and shields the
330 acrylamide functional groups from saponification in a highly alkaline environment. The
331 thermal stability and salt tolerance of VSVA copolymers-in a low clay content, low solid
332 content, high electrolyte concentration drilling fluid were investigated. The VSVA polymer
333 improved fluid stability up to 400 ° F (204 ° C), retained good fluid loss control behaviour, and
334 provided stable rheology properties.

335 Hille (1985) investigated the effectiveness of a VSVA copolymer under elevated temperature
336 and high electrolyte concentration. The laboratory and field investigations revealed the
337 effectiveness of the copolymer to control filtration properties up to 392 ° F (200 ° C). The
338 rheological properties of VSVA based fluids remained stable when contaminated leading to
339 high concentrations of calcium and magnesium. This was due to electrostatic shielding of the
340 acrylate groups by the anionic and highly charged sulfonate moiety. Apart from filtration and
341 rheological improvements, the copolymer also minimized thermo-gelation. A well in North
342 Germany with a bottom hole temperature of 383 ° F (195 ° C) was drilled using VSVA treated
343 saltwater fluid. The VSVA copolymer provided excellent stability to the drilling fluid, and no
344 additional additives were required for 22 days of drilling.

345 ***AM-AMPS (AAM-AMPS) copolymer***

346 Qu et al. (2023) synthesised an AM/AMPS copolymer and found that the plastic viscosity of
347 the fluid after hot rolling at 464 ° F (240 ° C) was reduced by over fivefold. In contrast fluid loss
348 performances was still acceptable. A previous study was more systematic. Perricone et al.
349 (1986) synthesized two water-soluble copolymers of AM/AMPS and an alkyl-substituted
350 acrylamide monomer (AAM) using an ammonium persulfate initiated bulk polymerization
351 technique. The molecular weight of the copolymers ranged from 750 to 1500 kDa. It was
352 reported that the amide and vinyl group could hydrolyse under alkaline conditions, whereas
353 AAM provides resistance towards alkaline hydrolysis owing to the presence of the alkyl
354 functional group (methyl, ethyl). The AAM/AMPS copolymer did not depolymerize under the
355 hydrolytic and oxidative environment the drilling fluid was exposed to and did not form an
356 insoluble salt in the presence of an electrolyte. The effectiveness of the copolymer was
357 evaluated in a geothermal field with a downhole temperature exceeding 500 ° F (260 ° C).
358 Initially the drilling fluid employed used lignite and lignite derivatives; however, these were
359 found to be uneconomical in controlling the filtration losses at elevated temperature.
360 Therefore, the drilling fluid was treated with a copolymer to provide filtration stability. In
361 another well, the copolymer was utilized to control the filtration loss occurring during a coring
362 operation in a well with a bottomhole temperature exceeding 350 ° F (177 ° C). The copolymer

363 (AAM/AMPS) offered excellent core protection, and a permeability test indicated no
364 formation damage.

365 Eisen et al. (1991) formulated a lime-based drilling fluid system comprising a VSVA copolymer
366 and a low-molecular-weight polyacrylate terpolymer, lignosulfonate, and sulfonated asphalt
367 to drill a well in Mustang Island, Texas, having a bottom hole temperature of 338 ° F (170 °C)
368 The fluid was thermally stability up to 350 ° F (177 °C). Furthermore, the fluid also provided
369 enhanced stability under salt and CO₂ contaminations.

370 Audibert and Argillier (1995) investigated the chemical modification of polyacrylamides to
371 improve their thermal stability and the hydrolysis of acrylamide groups to acrylate groups by
372 incorporating AMPS/SSS/MA monomers in the polymer. The authors also evaluated the
373 stability of sulfonated polymers in a controlled environment. The study revealed that a typical
374 sulfonate polymer starts degrading at a temperature higher than 302 ° F (150 °C).

375 Kar *et al.* (2011) reported formulation of high-performance water-based fluids comprising
376 SSMA copolymer, AM-AMPS copolymer, and manganese tetraoxide (as dispersant, fluid loss
377 control agent, and weighting agent respectively). The formulated fluid was reported to be
378 thermally stable up to 392 ° F (200 °C).

379 ***Hydroxyl-sulfonated (HS) copolymer***

380 Plank and Hamberger (1988) developed a synthetic sulfonated polymer comprising hydroxyl
381 and sulfonic acid groups attached to the polymer backbone through alkene moieties. The low
382 pka of the sulphonate groups prevents the chelation of calcium cations ensuring calcium
383 tolerance greater than 200 g/L. The polymer containing drilling fluid was thermally stability
384 up to 320 °F (160 °C). The copolymer was also reported to reduce the HPHT filtration losses
385 of an offshore Gulf of Mexico well from 45 ml to 5.3 ml. The above-mentioned high
386 temperature and calcium resistant hydroxyl-sulfonated polymer was further utilized in
387 Zechstein wells in Germany. The polymer showed high electrolyte tolerance and was deemed
388 cost-effective. It was also found that the polymer increased the thermal stability of additives
389 such as lignite, starch, VSVA, and a polymer derived from cellulose (Ujma and Plank, 1989).

390 ***AA-AMPS copolymer***

391 Wilcox and Jarrett (1988) investigated the effect of a polymeric deflocculant comprised of AA
392 and AMPS comonomers on drilling grade clay and formation solids flocculation. It was
393 reported that the polymeric deflocculant improved the thermal stability of the fluid, provided
394 increased tolerance towards solids and electrolytes, and inhibited temperature induced
395 gelation of the fluid.

396 ***Poly alkylene glycol***

397 van Oort et al. (1997) proposed a new method to improve the thermal stability of
398 conventional rheology modifiers and fluid loss control polymers by introducing polyglycols to
399 the drilling fluid system. The authors evaluated three types of polyglycols: poly alkylene glycol,
400 polyethylene glycol, and fatty amine ethoxylate. The hydrophobic association between the

401 polymer chains and the polyglycol stabilized the polymer at elevated temperatures (320 ° F;
402 160 °C).

403 ***AM-NVP copolymer***

404 Tehrani *et al.* (2009a, b) reported the formulation of a high-density HPHT water-based drilling
405 fluid system comprised of clay and a terpolymer of AM, sulfonated monomer, and NVP. This
406 fluid had excellent fluid-loss control properties and provided thermally stable rheology. A
407 laboratory test indicated excellent fluid-loss control behaviour of the fluid formulation up to
408 450 ° F (230 °C). However, the fluid developed progressive gel strength, and therefore, the
409 addition of a dispersant was required. Qu *et al.* (2023) report a more than twofold reduction
410 in plastic viscosity after hot rolling at 464 ° F (240 °C) for a similar polymer. The authors state
411 that the pyrrole ring groups, is effective in improving the stability of the polymer at high
412 temperatures in aqueous solutions.

413 ***AM-SSS copolymer***

414 Recently Qu *et al.* (2023) have studied an AM/SS co-polymer-based fluid. After hot rolling 1t
415 464 F (240 C), the plastic viscosity was around half the room temperature value. It is
416 postulated that the polymeric prevents bentonite flocculation because of its high adsorption
417 on the clays thus stabilising the clay particles. Furthermore, the styrene sulfonate group
418 imparts thermal stability to the AM backbone.

419 ***AM-DMDAAC copolymer***

420 Lin and Luo (2015) synthesized a copolymer of AM and DMDAAC using ammonium persulfate-
421 sodium bisulfite redox reaction to initiate free-radical polymerization. The copolymer was
422 hydrolysed by treating it with sodium hydroxide. The thermal stability and salt resistance of
423 the hydrolysed copolymer were evaluated by formulating freshwater and salt water-based
424 fluids. The formulated fluid was thermally stable up to 392 ° F (200 °C) and had salt resistance
425 up to 30 wt% of NaCl.

426 ***Star-poly[AM-AMPS]***

427 Luo *et al.* (2018) synthesized a star-shaped copolymer of AM and AMPS using a multi-
428 functional macro-initiator. The copolymer was prepared in a three-step process. The
429 rheological and filtration performance of water-based drilling fluid formulated with
430 synthesized copolymer was evaluated at 320 ° F (160 °C). It was observed that the copolymer-
431 based fluid had better shear thinning behaviour and was more stable to high-temperature
432 shearing.

433 ***Terpolymers***

434 ***AM-AMPS- DI terpolymer***

435 Wu *et al.* (2002) developed a terpolymer comprising di-sodium itaconate (sodium salt of
436 itaconic acid), AM, and the sodium salt of AMPS using free radical polymerization. The
437 terpolymer was used to formulate fresh and saltwater-based fluids. The prime function of the
438 terpolymer was to act as a filtration loss control additive (by forming an impermeable filter

439 cake) under high-temperature conditions (428 ° F, 220 °C)). In addition, the terpolymer
440 behaved as a deflocculant. The stability of the saltwater-based fluid indicated a high salt
441 tolerance capacity for the terpolymer at high temperatures. This is attributed to the carboxyl
442 functional group of the DI monomer. The AM and AMPS improved clay dispersion, provided
443 enhanced salt tolerance, and aided in the formation of an impermeable filter cake to minimize
444 filtration losses at high temperatures.

445 ***AM-AMPS-VP terpolymer***

446 Cao *et al.* (2017) synthesized a pH-responsive copolymer comprising AM, AMPS, and VP via
447 ammonium persulfate initiated free radical polymerization. The comonomers AM, and VP acts
448 as adsorption groups, whereas the AMPS units provide anti-calcium chelation properties to
449 the copolymer. A freshwater-based fluid containing the synthesized copolymer and bentonite
450 was found to be exhibit stable rheology and filtration control at 300 ° F (149 °C)) and was also
451 found to be calcium resistant up to 20 wt%.

452

453 ***AM-AMPS- AA terpolymer***

454 Peng *et al.* (2010) synthesized a terpolymer of acrylic acid (AA), and AMPS using a potassium
455 persulfate–sodium bisulfite redox initiated free radical polymerization process. The
456 synthesized terpolymer was evaluated by formulating fresh water-based fluids comprising
457 bentonite and sodium bicarbonate. In addition, an aluminium citrate solution was also added
458 to stabilize the fluid at elevated temperatures. A laboratory test confirmed improvements in
459 fluid rheology and a decrease in filtration losses with the addition of terpolymer and
460 aluminium citrate solution. The drilling fluid was found to be stable up to 356 ° F (180 °C). It
461 was proposed that hydrophilic gels of low crosslink content are formed by the complexation
462 reaction of the terpolymer and the aluminium citrate. The bridging of aluminium cations
463 between the anionic terpolymer chains (which are negatively charged) and clay platelets
464 helps inhibit the loss of viscosity typically encountered during high-temperature drilling.

465 ***AM-AMPS-VA terpolymer***

466 Nagre *et al.* (2016) synthesized two acrylamide-based copolymers using a potassium
467 persulfate-sodium metabisulfite redox initiated free-radical polymerization. The first
468 copolymer (MWV: $4.75 \times 10^6 \text{ g mol}^{-1}$) consisted of AM, AMPS, and vinyl acetate (VA)
469 monomers (and was designated as CP4). The second copolymer (CP5: MWV: $4.56 \times 10^6 \text{ g}$
470 mol^{-1}) consisted of AM, sodium acrylate (NaA), N, N' dimethyl acrylamide (DMAM), and NVP.
471 The colloidal stability and salt tolerance of the synthesized copolymers at elevated
472 temperatures was evaluated by formulating a freshwater-based fluid. The acrylamide-based
473 polyelectrolytes enhanced the rheological properties of drilling fluid systems at temperatures
474 up to 300 ° F (149 C)). The comonomer AM improves the dispersion of bentonite particles and
475 acts as a bulk viscosifying agent, whilst AMPS provides hydrolytic stability and resistance
476 towards salt contamination. The drilling fluid exhibited stable rheology in salt concentrations
477 of 20 wt% NaCl, 2.0 wt% MgCl₂, and 2.0 wt% CaCl₂.

478 ***AM-AMPS-ionic liquid polymer***

479 Yang *et al.* (2017) reported the synthesis of an ionic-liquid-based copolymer (PASV) via 2,2'-
480 azo-bis (2-methylpropionamidine) dihydrochloride (AAPH) initiated free-radical
481 polymerization. The imidazole unit of the ionic liquid provides thermal stability, and the
482 cationic quaternary ammonium group protects against calcium contamination. The other
483 comonomer AM helps in rheological control at elevated temperature by increasing the
484 thickness of the hydration layer, whereas the sulfonic group of AMPS helps in filtration and
485 salt tolerance. The synthesized IL-based copolymer was evaluated for filtration loss control
486 and calcium salt tolerance properties by formulating a freshwater-based fluid with calcium
487 contaminants and thermally aging at 356 °F (185 °C). The copolymer was found to control
488 filtration loss when aged up to 356 °F (185 °C) and calcium contamination up to 11 wt%.

489 ***AM-AMPS-SSS terpolymer***

490 Huo *et al.* (2018) synthesized a terpolymer comprising of SSS, AM, and AMPS monomer
491 through an inverse emulsion polymerization. The non-ionic amide units from AM and sulfonic
492 acid groups from AMPS and SSS favoured adsorption on clay particles resulting in a well
493 dispersed fluid system at high temperature. The formulated drilling fluid showed improved
494 rheology at high temperature (arising from the phenyl group of SSS). The improved resistance
495 to flocculation of the clay at high temperatures improved the filtration properties of the
496 system. The rheological and filtration parameters of formulated copolymer-based fluid were
497 not significantly affected by thermal aging at 320 °F (160 °C). The micro-structural analysis
498 revealed that the reduction in filtration losses was aided by physical plugging of the porous
499 medium by the copolymer.

500 ***AM-AMPS-NVP terpolymer***

501 Mao *et al.* (2020) synthesized an anionic polymer comprising AM, AMPS, and NVP using 2, 2'
502 -Azobis(2-methylpropionamidine) dihydrochloride (AAPH) initiated free radical
503 polymerization. The polymer was used to formulate a water-based drilling fluid. The
504 formulated polymer-based fluid was found to be resistant to chlorine and calcium ion
505 contamination (resistant up to 4.5×10^5 ppm and 4×10^5 ppm, respectively) after thermal
506 aging at 356 °F (180 °C). Owing to the presence of the sulfonic acid group (AMPS monomer)
507 and pyrrolidine group (NVP monomer), the synthesized polymer exhibited a stronger
508 interaction with bentonite particles under high-temperature conditions leading to
509 improvement in the colloidal dispersion of the clay in the drilling fluid.

510 ***AM-AMPS-VI (AAV) terpolymer***

511 Aghdam *et al.* (2020) synthesized a polymeric fluid loss control agent comprised of monomer
512 AM, AMPS, and 1-vinyl imidazole (VI) using radical polymerization in the presence of
513 potassium persulfate initiator. The fluid loss control properties were evaluated by thermally
514 aging a water-based drilling fluid containing AAV at 365 F (180 °C). The filtration loss volume
515 was found to be in the range of 1.4 ml–6.5 ml with thinner filter cake in the range of 0.21
516 mm–0.79 mm. The fluid control mechanism of the AAV copolymer was attributed to the

517 deflocculation of bentonite particles, surface adsorption onto bentonite particles and the
518 formation of a chelate complex with cations.

519 ***Quadripolymers***

520 ***AM-AMPS NVP-SSS- quadripolymer***

521 Li *et al.* (2014a, b) synthesized a quadripolymer comprising AM, AMPS, SSS, and NVP via
522 redox-initiated free radical polymerization. The quadripolymer was found to effectively
523 control the filtration loss of a freshwater-based fluid when subjected to an aging temperature
524 of 392 ° F (200 °C). The high-temperature stability of the polymer is attributed to the
525 presence of hydrophobic pyrrolidine and phenyl functional groups on the NVP and SSS
526 monomers. Drilling fluid samples treated with salt to mimic fluid contamination showed
527 reduced viscosity owing to aggregation of the polymer. However, filtration loss volume was
528 unaffected, confirming a degree of salt resistance for the polymer. The filtration behaviour
529 was attributed to the adsorption of the polymeric chains on bentonite in the fluid. In addition,
530 the adsorption behaviour of polymer was characterized using AFM. The AFM analysis showed
531 uniformly dispersed polymer on the bentonite surface with formation of a networked
532 structure.

533 ***AM-AMPS-NVP-DMDAAC quadripolymer***

534 Su *et al.* (2014) synthesized a quadripolymer comprising AM, AMPS, NVP, and DMDAAC using
535 potassium persulfate-sodium bisulfate redox initiated solution free radical polymerization.
536 This resulted in a polymer with an average molecular weight of 530 000 Da. The thermal
537 stability and salt tolerance of the polymer were evaluated by formulating a salt saturated
538 brine-based fluid. After thermal aging, the fluid showed stable rheology and filtration loss
539 behaviour up to 356 ° F (185 °C). The fluid loss control behaviour of the polymer was
540 compared with an AM-AMPS-NVP terpolymer. It was observed that the quadripolymer
541 controlled fluid loss volume better than the terpolymer. The thermal stability of the
542 quadripolymer is attributed to the incorporation of hydrophobic temperature-resistant
543 pyrrolidine functional groups in the polymer (introduced by the NVP monomer). In addition,
544 the DMDAAC monomer favours the formation of a pyrrolidine structure during
545 polymerisation, thereby further increasing thermal stability. It is postulated that the
546 quaternary ammonium group of the pyrrolidone inhibits the swelling of clays and hence
547 improves the quality of the filter cakes formed leading to effective control of fluid loss.

548 ***AM-AMPS-DMDAAC-SSS quadripolymer***

549 Bai *et al.* (2015) synthesized a quadripolymer comprising AMPS, AM, DMDAAC, and SSS via an
550 ammonium persulfate initiated free-radical solution polymerization reaction. Monomers such
551 as AMPS and SSS bear sulfonic acid groups which improve the salt tolerance of the fluid. The
552 phenyl group from SSS provides rigidity to the polymer backbone and hence improves the
553 thermal stability of the polymer. DMDAAC acts to inhibit flocculation of bentonite and hence
554 improves the quality of the filter cakes formed leading to a decrease in filtration loss. The
555 selection of the monomers was optimized using an orthogonal design of experiments
556 approach. The rheological and filtration loss behaviour of the quadripolymer was evaluated

557 by subjecting the formulated drilling fluid to thermal aging. The results indicated that
558 rheological and fluid loss properties of the drilling fluid are stable up to 356 °F (180 °C).

559 Huang *et al.* (2019b) reported the synthesis of a quadripolymer also comprising AM, AMPS,
560 DMDAAC, and SSS made via free-radical aqueous solution polymerization. The thermal
561 stability and salt tolerance behaviour of the polymer-based fluid were evaluated at HPHT
562 conditions. It was observed that the polymer imparted stable rheology up to 464 °F (240 °C),
563 and salt-resistance up to 30 wt% NaCl. The high-temperature stability is attributed to the
564 phenyl and pyrrolidine structure of the quadripolymer. However, the polymer was not able
565 to resist CaCl₂ contamination. The filtration control of the polymer was compared with
566 commercial additives and was found to be more effective in controlling filtration loss.

567 ***AA-AMPS-MA-DMDAAC quadripolymer***

568 Huang *et al.* (2015) synthesized a quadripolymer comprising AA, AMPS, DMDAAC, and MA
569 monomers via ammonium persulphate initiated free-radical polymerization. The
570 polymerization conditions and initiator dosage were optimally selected to obtain a low
571 molecular weight quadripolymer (M_{WW}: 8036 Da, M_{WN}: 8107 Da). A freshwater based
572 drilling fluid comprising sodium carbonate, calcium bentonite, clay, and quadripolymer was
573 prepared to assess the thinning properties of the quadripolymer. The results were also
574 compared with a commercial thinner. The quadripolymer was found to reduce the viscosity
575 of the fluid up to 473 °F (245 °C)). The viscosity reduction is attributed to the presence of
576 cationic moieties (DMDAAC) and strongly hydrated groups (AMPS), resulting in polymer
577 adsorption on the calcium montmorillonite (Ca-Mt), thus providing strong hydration and
578 swelling inhibition.

579 ***AM-AMPS-SSS-METAC quadripolymer***

580 Xiping *et al.* (2016) synthesized a quadripolymer comprising AM, AMPS, SSS, and METAC
581 monomers using ammonium persulfate-initiated solution polymerization. The cationic
582 quaternary ammonium and tri methyl end groups prevent clays from flocculating, and the
583 sulfonic acid group (SO₃⁻ Na⁺) from the AMPS and SSS monomers provides a high degree of
584 hydrophilicity to the polymer and thus, improves salt tolerance. The resonance stabilized
585 benzene ring of SSS imparts heat resistance to the polymer. The quadripolymer was evaluated
586 by formulating a freshwater, a saturated saltwater, and a composite-brine drilling fluid. The
587 API filtration loss was found to be 5.2 mL whilst the HPHT filtration loss at 392 °F (200 °C) was
588 found to be 10.6 mL, indicating effective filtration loss control.

589 ***AM-AMPS-NVP-DHBS quadripolymer***

590 Chu and Lin (2019) synthesized a polymer (PAAND) comprised of AM, AMPS, NVP, and
591 potassium 2,5-dihydroxy benzene sulfonate (DHBS) by introducing the phenyl group in the
592 backbone of copolymer through horseradish peroxidase (HRP) mediated RAFT
593 polymerization. The rheological and filtration properties of the copolymer-based fluid were
594 evaluated by thermal aging at 464 F (240 °C). The efficiency of controlling rheology and
595 filtration loss at high temperature was found to follow the order: PAAND > PAANS > PAAN

596 copolymer. The incorporation of rigid DHBS monomer in the backbone of copolymer
597 improved rheological stability and filtration control at high temperatures.

598 ***AM-AMPS-HEMA-LMA quadripolymer***

599 Nagre *et al.* (2021) synthesized a hydrophobically associating heteropolymer (HAH)
600 comprising AM AMPS), HEMA, and LMA using micellar radical polymerization. The monomer
601 AM was selected to provide viscosifying behaviour to the polymer, whereas AMPS imparted
602 a high anionic charge and offering temperature and salt tolerance. The monomer HEMA was
603 added to increase the water retention capacity of polymer to decrease filtration losses. LMA
604 provided allowed hydrophobic association in saline media and inhibited chain collapse. The
605 filtration behaviour of a HAH-containing water-based drilling fluid was studied in the
606 temperature range of 25–160 °C. The polymer maintained excellent filtration control with a
607 fluid loss volume of 8.4–8.6 ml compared with 43.5–107.0 ml for polymer-free fluids. In
608 addition, the salt contaminated fluid was also found to impart stable rheology with API
609 filtration loss of 7.6–8.8 ml after hot rolling at 302 °F (150 °C).

610 ***AM-AMPS -NVP-IA quadripolymer***

611 Wu *et al.* (2001) synthesized a copolymer comprising of NVP, IA, AM, and AMPS using free
612 radical polymerization. A laboratory test of a formulated freshwater-based fluid comprising
613 bentonite, sodium carbonate, and the synthesized copolymer, confirmed the excellent
614 filtration control properties of the copolymer up to a temperature of 428 °F (220 °C). The high-
615 temperature resistance of the copolymer is attributed to the cyclic pyrrolidone unit of the
616 NVP monomer. In addition, the anionic sulfonate group binds with clay particles stabilising
617 the clay and keeping particles deflocculated. The improved filtration behaviour was attributed
618 to the large chain length of the polymer.

619 ***AM-AMPS-SSS-DMDAAC quadripolymer***

620 Wang et al. (2022) synthesised a quadripolymer comprised of AM, AMPS, SSS and DMDAAC.
621 The effect of hot rolling at different temperatures was studied and it was found that the
622 viscosity of the formulated fluids was relatively stable up to 356 °F (180 °C), thereafter there
623 was a considerable reduction in viscosity. At 428 °F (220 °C), the apparent viscosity was
624 reduced by around 75%.

625 ***DMAA-AMPS-DMDAAC-NVCL quadripolymer***

626 Li *et al.* (2022) report synthesising a zwitterionic quaternary copolymer comprised on DMAA,
627 AMPS, DMDAAC and NVCL. After hot rolling a fluid containing the novel polymer at 428 °F
628 (220 °C), the filtration loss of the fluid was only 6.5 ml. The apparent viscosity, in both the
629 absence and presence of salt, was reduced by only around one third. The apparent viscosity
630 was hardly impacted in the absence of but reduced by up to one third at the highest salt
631 concentration (36%).

632 ***Branched polymers***

633 ***AM-SSS-APET terpolymer***

634 Yan *et al.* (2013) synthesized an amphiphilic comb-shaped terpolymer of AM, SSS, and allyl
635 polyoxyethylene-12 ether (APET) using an inverse microemulsion polymerization technique.
636 The amide and polyoxyethylene units of the terpolymer improved clay dispersion by forming
637 intermolecular hydrogen bonds with clay particles and helped to develop a networked
638 structure. The negatively charged sulfonic acid group improved the colloidal stability of fluid.
639 It was proposed that the high hydration ability of the sulfonic acid groups inhibits damage to
640 the hydration shell of the bentonite under high temperature and salinity conditions. In
641 addition, the unique comb-like structure also favours the formation of networked structures
642 and helps in the reduction of salt screening. For the evaluation of the polymer, a low solid
643 drilling fluid comprising bentonite, sodium bicarbonate, and polymer was prepared and
644 laboratory tested under high temperature and high salinity conditions., The zeta potential of
645 the clay particles in an aged sample (at 302 F. 160 °C) of the fluid was measured and found
646 to be – 31.1 mV, indicating colloidal stability of the clay. Furthermore, the formation of a
647 networked structure between bentonite and terpolymer ensured the formation of compact
648 filter cake and low filtration volume under high temperature and salinity conditions.

649 ***AMPS- NVP-SSS- APEG terpolymer***

650 Liu *et al.* (2018) synthesized a comb-shaped copolymer of AMPS, NVP, SSS, and allyl
651 polyoxyethylene ether (APEG) by free radical polymerization. The APEG chains imparted steric
652 hindrance and helped in controlling colloidal aggregation of clay at high temperatures and
653 under high salinity conditions. The other comonomers, AMPS, and SSS offered an ionizable
654 sulfonic acid group that increases the hydration shell around the clay particle and improves
655 salinity tolerance. In addition, the ring structure from NVP and SSS monomers helped to
656 enhance the rigidity of the main chain and improved temperature tolerance. The filtration
657 control behaviour of the polymer was evaluated by aging the fluid at 392 ° F (200 °C). The fluid
658 loss volume was found to be less than 10 mL, indicating the effectiveness of polymer in
659 controlling fluid loss at elevated temperatures. The salt tolerance of the polymer was
660 evaluated by adding variable loadings of salt contaminants to the fluid and thermal aging at
661 356 ° F (180 °C). A fluid loss volume of fewer than 15 ml was observed with a contamination
662 of 10.0 wt% NaCl and 1.0 wt% CaCl₂, indicating excellent salt tolerance for the polymer.

663 ***Crosslinked polymers***

664 Long linear polymers have limited tolerance to salt contamination and shear sensitive (i.e.,
665 can be degraded at high shear rates). Compared with linear polymers of similar molecular
666 weight, crosslinked polymers have smaller hydrodynamic volumes. This property results in
667 crosslinked polymer being sterically hindered which increases hydrolytic (thermal) stability
668 (Thaemlitz *et al.*, 1999). The smaller size of the polymer also makes them more shear resistant
669 and the crosslinking makes the polymer less sensitive to solid contaminants.

670 ***AMPS-NVCL-DVB terpolymer***

671 Xie *et al.* (2016) synthesized a copolymer (SDKP) comprised of AMPS, and NVCL monomers,
672 crosslinked with di-vinyl benzene (DVB) using 2,2-Azobisisobutyronitrile (AIBN) initiated
673 micellar radical polymerization. The synthesized cross-linked polymer was evaluated by

674 formulating a low-solid freshwater base drilling fluid. The polymer displayed a thermo-
675 thickening effect in a temperature range of 302–356 ° F (150–180 °C), providing good viscosity
676 control and compensating for the thermal thinning of drilling fluids at elevated temperatures.
677 The fluid was found to provide resistance towards elevated temperature up to 446 °F (230 °C)
678 and salt tolerance up to 8.0 wt %.

679 ***AM-AMPS-AHPS-AA terpolymer***

680 Sepehri *et al.* (2018) studied the effect of crosslinking agent, transfer agent, and co-monomer
681 loading on the fluid loss and rheological properties of the resulting polymer. The first
682 terpolymer (CP1) was synthesized by solution polymerization and consisted of AM, AMPS,
683 and NVCL monomers. It was observed that the cross-linked polymer offered better fluid loss
684 control than a linear polymer. However, it was also reported that cross-linker increased the
685 viscosity and decreased the solubility of the polymer. Additionally, the effect of the chain
686 transfer agent was also evaluated. It was found that an increase in chain transfer agent
687 reduced molecular weight and viscosity; however, fluid loss volume was increased. It was also
688 observed that an increase in AMPS content also increased fluid loss volume but increased salt
689 tolerance. The AM units contain –CONH₂ groups that enhance interaction with bentonite to
690 provide helping disperse the clay particles and improving the high temperature viscosity of
691 the drilling fluid. The sulfonic acid group of the AMPS monomer provides salt tolerance. In
692 addition, the rigid lactam group from NVCL improves the thermal stability of the polymer. The
693 second copolymer (CP2) comprised AM, AMPS, AHPS, and AA monomers. The effect of CP1 &
694 CP2) on thermal stability and filtration control was evaluated in a water-based drilling fluid. It
695 was reported that CP2 led to lower filtration loss volumes than CP1 after thermal aging at 302
696 ° F (150 °C) (this was possibly owing to the presence of a long side chain of poly-acrylic acid in
697 CP2). The salt tolerance and fluid loss control performance of the polymers were better than
698 starch.

699 ***Crosslinked AA-AMPS polymer***

700 Gang *et al.* (2020) synthesized a deformable plugging polymer (DPP) by crosslinking AA and
701 AMPS with MBA crosslinker. DPP showed a strong water swelling capacity and pressure
702 sealing ability up to a temperature of 302 ° F (160 °C). The DPP was applied to 8 wells of a gas
703 field in China to demonstrate the ability of DPP to plug the leaking formation.

704 ***Crosslinked AM-MBA microgel***

705 Wang *et al.* (2020) synthesized a cross-linked microgel (CMG) polymer of monomer AM and
706 crosslinker MBA using dispersion polymerization. The results indicated that the CMG polymer
707 showed excellent thermal stability (up to 392 °F; 200 °C)). Transmission electron microscope
708 images of the CMG polymer show spherical and oval shapes around a micron in length. The
709 influence of initiator concentration and crosslinking agent on particle size was evaluated. The
710 results revealed that the size of CMG polymer increases with an increase in initiator loading,
711 whereas the size decreases with increase in crosslinking agent concentration.

712 ***Graft copolymers of natural materials***

714 Lignite is a low value coal. It is typically utilized as a thinner, filtration loss control agent,
715 emulsifier, and rheology stabilizer in oil and gas well drilling (Fink, 2012). The stabilizing
716 behaviour of lignite is attributed to the presence of humic acids and the associated carboxylic
717 groups (Gavrilof and Koledin, 1999). It is believed that the hydrophilic carboxylic acid and
718 phenolic groups in humic acid bind with clay platelets to keep the clays deflocculated and
719 inhibit thermal-gelation of the fluid. Additionally, humic acid forms complexes with ions such
720 as Mg^{2+} , Ca^{2+} , and Fe^{3+} , therefore offering salt resistance. The phenol ring-based moieties
721 stabilise the polymer chains, and the inflexible ring structure enhances the thermal stability
722 of the polymer. However, lignite-based fluids are susceptible to contamination from calcium
723 compounds and from other common salts (Monroe, 1962). In addition, these fluids require a
724 high alkalinity during formulation and application (Monroe, 1964). These shortcomings were
725 addressed by the development of chemically crosslinked sulfomethylated lignite polymer
726 (Dorman, 1991). The polymer was laboratory tested and was found to provide rheological and
727 filtration control up to 437 °F (225 °C). A field gypsum-based fluid was treated with modified
728 lignite and aged at 356 °F (180 °C). The laboratory test revealed that the addition of modified
729 lignite reduced thermal gelation and reduced filtration loss.

730 Shen and Zhang (2018) reported the synthesis of lignite graft sulfomethyl phenol aldehyde
731 polymer by polycondensation using formaldehyde and phenol. The effect of the polymer on
732 the rheological and filtration properties of a bentonite slurry were evaluated. The polymer
733 was found to effectively reduce the fluid loss at temperature up to 392 °F (200 °C) and also
734 regulated the rheological properties of the drilling fluid. The synthesized lignite-based graft
735 polymer was a more effective fluid loss control agent than the commonly used causticized
736 lignite additive.

737 ***Polyanionic cellulose graft AM-AMPS-SSS (PAC-g-AAS)***

738 Poly anionic cellulose (PAC) has a molecular carboxymethyl unit (i.e., $-CH_2COO-Na^+$). As the
739 primary hydroxyl group is more reactive than the secondary hydroxyl group, the primary
740 hydroxyl group is generally involved in carboxy methyl substitution. The functional groups
741 associated with PAC are carboxyl and hydroxyl. As indicated, a carboxyl group is responsible
742 for the salt (e.g., calcium and magnesium) and acid resistance of the polymer (i.e., there is no
743 precipitation of PAC under salt contamination and acidic pH). In addition, the carboxyl group
744 has a strong binding capacity with water and assists in forming a gel. Hydroxyl groups
745 (secondary) have a strong water sorption capacity and form hydrogen bonds with the
746 neighbouring glucose unit.

747 Owing to the presence of a hydrophobic polysaccharide backbone and many pendant
748 hydrophilic carboxyl groups, PAC exhibits amphiphilic behaviour. PAC also displays
749 exceptional filtration and rheological control behaviour under wide temperature variations.
750 However, PAC cannot be used beyond 392 °F (225 °C) because of biodegradable cellulose
751 units in the molecule.

752 Gautam and Guria (2020a) synthesised a PAC graft AM, AMPS, and SSS copolymer using free
753 radical polymerization. In the PAC grafted AM-AMPS-SSS polymer, individual monomers have
754 a specific role in improving the property of the drilling fluid under high temperature, saline,
755 and acidic conditions. Therefore, an optimal combination of the functional groups from the
756 AM, AMPS, and SSS monomers, should result in an excellent HT drilling fluid. The PAC grafted
757 copolymer was used to prepare HPHT drilling fluids containing bentonite and functionalized
758 fly ash (Gautam et al., 2018). The resulting fluid had enhanced rheology control, filtration
759 characteristics, and lubricity at temperatures up to 437 °F (225 °C). Furthermore, the fluid
760 remained stable (with adequate rheology, fluid loss, and lubrication properties) in solutions
761 of NaCl (4.6 wt%) and CaCl₂ (4.4 wt%), and under acid contamination (pH: 6.5).

762 ***Environmental aspects***

763 The selection of a drilling fluid generally depends on the downhole conditions of the well
764 being drilled, its geographical location, and the prevailing environmental legislation. The oil
765 and gas drilling industry has shifted towards low toxicity and readily biodegradable synthetic
766 and water-based fluids to minimize the environmental effects (Fadairo et al., 2012). However,
767 several other synthetic constituents are required to achieve high-temperature stability,
768 desired rheological, and filtration properties at elevated temperature conditions. These
769 synthetic additives can be toxic and pose severe threats to planktonic and marine organisms
770 if disposed of untreated and may also enter humans through the food cycle (Balgobin et al.,
771 2012; Landrigan et al., 2020; Pereira et al 2022).

772 The influence of the monomers used in the synthesis of polymers on the environment and
773 ecosystems, including human health, are of particular concern. For example, NVP monomer
774 is categorized in the highest hazard class, whereas AMPS is categorized in the lowest hazard
775 class (Lithner et al, 2011; Belgacem and Gandini, 2008). When developing new polymers, it
776 is therefore important to select component monomers with the lowest possible toxicity.

777 **Solid Fluid Modifiers**

778 ***Clay particles and modified clay particles***

779 ***Laponite***

780 Laponite is a synthetic hectorite clay with a disk-shaped structure. It has a diameter of 25 nm
781 and a thickness of 1 nm (Xiong et al., 2019). Laponite nanoparticles offer highly diversified
782 mechanical, chemical and structural properties along with surface charge, morphology, and
783 biodegradability (Das et al., 2019). Xiong et al. (2019) evaluated the thermal resistance,
784 viscosifying behaviour, and salt tolerance capabilities of laponite. The experimental results
785 revealed that the laponite has excellent viscosifying abilities and can function at a
786 temperature of up to 260 °C. The viscosifying effect of laponite was compared with
787 commercial viscosifier HE300 and DRISCAL–D, and it was found that laponite performed
788 better at retaining viscosity at high temperatures.

789 ***Laponite graft AM-AMPS-DMDAAC***

790 Huang *et al.* (2019a) studied the effect of laponite nanoparticles on the thermal stability of a
791 synthetic polymer-based fluid. First, a terpolymer (AAD) of AM, AMPS, and DMDAAC was
792 synthesized through radical polymerization. Then laponite nanoparticles were added to
793 formulated AAD based fluid. The experimental results suggested that laponite was beneficial
794 in maintaining a higher viscosity and slowing down the degradation of the AAD terpolymer
795 owing to strong electrostatic interactions and hydrogen bonding between laponite and
796 functional groups of AAD. The formulated nano-laponite and synthetic polymer-based fluid
797 were found to impart stable rheology up to 410 °F (210 °C).

798 ***Laponite graft AM-AMPS-DMDAAC-S***

799 Shen *et al.* (2020) synthesized a hydrophobic associated polymer (AADS–LP) based laponite
800 composite by in situ emulsion polymerization of monomers: AM, AMPS, DMDAAC, ST, and
801 laponite. Morphological analysis using SEM, revealed a bean pod-like structure which was
802 beneficial in filtration loss control. The addition of AADS–LP in freshwater-based fluid
803 improved rheology, salt tolerance, and filtration properties under high-temperature
804 conditions (302 °F; 160 °C). The polymer (AADS–LP) is absorbed on to the clay surfaces (by a
805 combination of electrostatics and hydrogen bonding) which hydrates the clay surface
806 preventing aggregation of the clay particles at high salinities. The improvement in filtration
807 properties was attributed to blocking pores and cracks and forming a smooth layer of clay at
808 the surface.

809 ***Laponite graft AM-AMPS-DMDAAC-ACMO***

810 Yang *et al.* (2022) synthesised a laponite grafted polymer composite consisting of AM, AMPS,
811 DMDAAC) and 4-acryloylmorpholine (ACMO). The apparent viscosity and yield point of a
812 water-based mud containing the polymer composite showed an upward trend with the
813 increasing temperature; this was irreversible. It was postulated that since as the aging
814 temperature increases, the thermal motion of water molecules increases, the hydration shell
815 on the particle (laponite and bentonite) surface becomes thinner, and the because of the
816 increased Brownian motion of the particles leads to more collisions to the aggregation of the
817 bentonite and laponite particles, resulting in an increase in particle size. The rheological
818 properties of mud decreased significantly above 248 °F (120 °C). The apparent viscosity value
819 was only 12 mPa·s at 392 °F (200 °C), a reduction of 90%. The authors postulate that high
820 temperature induced polymer oxidative degradation, conformational transformation, and
821 rupturing of hydrogen bonds, occurs which weakens the network structure and reduces the
822 viscosity of the drilling fluids.

823 ***Palygorskite (Pal)***

824 Palygorskite is a monoclinic phyllosilicate of magnesium and aluminium. The elongated shape
825 of the palykorskite particles helps in dispersion, salt and alkali resistance, and high-
826 temperature stability of drillings formulated with palykorskite. Abdo and Haneef (2013)
827 evaluated the application of palygorskite in HPHT oil and gas drilling. The Pal nanoparticles
828 were purified, synthesized, and further functionalized to tailor their effectiveness in

829 controlling bentonite dispersion. It was found that Pal considerably improved the thermal
830 stability of the fluid thus reducing the need for expensive rheology modifiers.

831 ***Sepiolite***

832 Sepiolite is a complex magnesium silicate with a fibrous texture and offers unique structural
833 characteristics and physio-chemical properties owing to the presence of molecular-sized
834 channels and grooves. Carney and Meyer (1976) evaluated sepiolite as an additive for HPHT
835 well drilling. The fluid formulation showed enhanced rheological stability up to 560 °F (290
836 °C); however, the reported fluid loss was high (>15 ml) owing to the spherical shape of
837 sepiolite. However, adequate filtration control can be achieved with the addition of synthetic
838 polymers and bentonite. Bannerman and Davis (1978) formulated a sepiolite-based fluid
839 which had better rheology control than a bentonite-lignite system. However, to achieve a
840 high yield point, prolonged shearing was required. Owing to the lack of filtration control by
841 macro-sized sepiolite, Abdo et al. (2016), synthesized nano-sepiolite with a 30–60 nm particle
842 size. These authors evaluated the effect of nano-sepiolite on the rheological and filtration
843 behaviour of bentonite-based fluid under HT condition. The PV and YP of the bentonite-based
844 fluid were found to improve by the addition of sepiolite in a temperature range of 50–180 °C.
845 The addition of sepiolite caused a 15% reduction in fluid loss volume.

846 ***Nanoparticles***

847 Nanoparticles (NPs) are engineered materials with at least one dimension in the range of 1–
848 100 nm (Cheng, 2014). The functional properties of nanoparticles are typically attributed to
849 their size, morphology, surface characteristics, and inner structure. The enhanced
850 physicochemical properties and colloidal stability of NPs are ascribed to the very small size
851 and extremely high surface-to-volume ratio (Vryzas and Kelessidis, 2017). Recent studies on
852 NPs have been demonstrated their capabilities to improve rheological properties, reduce
853 filtration loss and friction, increase the rate of heat transfer, alleviate shale instability and
854 inhibit gas hydrate formation (Rafati et al., 2018; Ali et al., 2020; Al-Shargabi et al., 2022; Oseh
855 et al., 2023).

856 ***Nano-silica and associated copolymers***

857 Silica (silicon dioxide) nanoparticles are hydrophilic in nature and possess spherical
858 morphology, high specific surface area, high thermal and mechanical properties. Apart from
859 this, the shape, size, surface charge, and roughness of silica nanoparticles can be tuned for
860 specific applications (Al-Shargabi et al., 2022). In light of the comprehensive reviews by Al-
861 Shargabi et al. (2022), and Oshe et al. (2023) we focus here only on nanoparticles
862 demonstrated to improve the high temperature rheological behaviour of drilling fluids.

863 ***Silica graft-p-[AM-AMPS-MA-ST]***

864 Mao *et al.* (2015) synthesized a novel hydrophobic associated polymer-based silica
865 nanoparticle with a core-shell structure (SDFL). The 1.0 wt% SDFL based WBM exhibited stable
866 rheology after thermal aging at 446 °F (230 °C) for 16 h with minimal reduction on apparent
867 viscosity and yield point. Moreover, the SDFL polymer composite exhibited excellent filtration

868 control with API filtration loss and HPHT filtration loss of aged fluid found to be 4.8 and 18.0
869 ml, respectively. Further, a 93.4% reduction in friction was observed for WBMs incorporating
870 SDFL. This was attribute to efficient plugging by micropores which form a multi-level network
871 structure.

872 ***Silica graft-AM-AMPS***

873 An *et al.* (2016) synthesized a nanoparticle-based fluid loss control agent by grafting a
874 acrylamide-based copolymer (AM-AMPS) onto modified silica. The modified nano-silica was
875 prepared by reaction of a silane coupling agent and thereafter nano-silica graft copolymer
876 was synthesized using surface-initiated free radical polymerization of modified nano-silica,
877 AM, and AMPS. Average particle size and thickness of copolymer were determined using TEM
878 and AFM analysis and were found to be 20 nm and 7.42 nm, respectively. The graft copolymer
879 provided resistance against salinity (up to salt saturation), calcium (up to 1 wt%), and high
880 temperature rheology (up to 302 ° F, 160 °C) in the formulated drilling fluids.

881 ***Silica graft DMAM-AMPS-MTAC polymer (NS-DAD)***

882 Sun *et al.* (2020) synthesized a salt responsive zwitterionic polymer comprising silica
883 nanoparticles, dimethylacrylamide (DMAM), AMPS, and 2-(Methacryloyloxy)ethyl
884 trimethylammonium chloride (MTAC). SEM images of the NS-DAD polymer revealed a well
885 dispersed and regular NPs of size 39 nm, whereas TEM image revealed interwoven needle-
886 like morphology indicating successful grating of polymers onto the surface of modified nano-
887 silica. The influence of polymer on water-based fluid was evaluated by varying dosage with
888 hot rolling at temperature 302 ° F (160 °C) for 16 h. A filtration loss volume of 5.8 ml was
889 observed for polymer-based hot rolled fluid, which was 97.01% less than polymer-free fluid
890 sample indicating the effectiveness of polymer to control HPHT filtration loss. The mechanism
891 for effective filtration control was the adsorption of NS-DAD on the clay surface to form a
892 stable spatial network structure and effectively plug the nanopore in the filter cake.
893 Additionally, the NS-DAD was found to impart stable rheology and filtration characteristics to
894 a saturated salt water-based fluid at 150 °C owing to the shielding of electrostatic interactions
895 of the molecular chain of the polyzwitterion resulting in a change of molecular structure from
896 a collapsed sphere to open helix.

897 ***Multiwalled carbon nanotubes (MWNCT)***

898 Multi-wall carbon nanotubes (MWCNTs) consist of nested single-wall carbon nanotubes¹
899 weakly bound together by van der Waals interactions in a tree ring-like structure. Multi-wall
900 carbon nanotubes are also sometimes used to refer to double- and triple-wall carbon
901 nanotubes (Iijima, 1991). MWCNT exhibits remarkable tensile strength (Yu et al., 2000),
902 thermal conductivity (Sadri et al., 2014), enhanced elastic modulus (Kumar et al., 2015), and
903 can be easily functionalized further to enhance rheology and filtration loss control. Abduo et

¹ Single-wall carbon nanotubes are one of the allotropes of carbon, intermediate between fullerene cages and flat graphene, with diameters in the range of a nanometre. Although not made this way, single-wall carbon nanotubes can be idealized as cut-outs from a two-dimensional hexagonal lattice of carbon atoms rolled up along one of the Bravais lattice vectors of the hexagonal lattice to form a hollow cylinder.

904 al. (2015) reported surface functionalization of MWCNT with a hydrophilic functional group.
905 A conventional WBM was treated with functionalized MWCNT. It was observed that the
906 addition of functionalized MWCNT to the drilling fluid system improved the thermal stability
907 up to 500 ° F (260 °C). Additionally, the fluid systems were found to be free from any
908 environmentally harmful materials. Ismail et al. (2016) investigated the applicability of
909 MWCNTs as a primary additive to control drilling fluid performance. The MWCNTs were found
910 to act as a rheology modifier and improved rheological properties such as PV, YP, and gel
911 strength. Later, Ismail et al. (2018) investigated the lubrication behaviour of MWCNT and
912 reported a 38–59% reduction of torque lubricity.

913 ***Lignosulfonate (LS) and associated copolymers***

914 The lignosulfonates are a complex mixture of polymeric compounds typically comprising an
915 aromatic ring, hydroxyl group, and sulfonate functional group attached to the propyl side
916 chain. The aromatic rings provide hydrophilicity and improve thermal stability. The sulfonate
917 group imparts ionic character and offers salt tolerance. The hydroxyl group provides sites for
918 oxidative hydrogen abstraction resulting in the formation of LS radicals which initiate graft
919 polymerization. The primary mechanism of lignosulfonate as a rheology modifier (thinner) is
920 to prevent the bentonite clay platelets from bonding together by satisfying the charge at the
921 edge of the clay plate and, therefore, eliminating the attractive electrostatic attraction
922 between the clay particles. Despite being widely adopted, it has several technical limitations.
923 These are: thermal degradation at temperatures greater than 250 ° F (121 °C) (Kelly, 1965),
924 induced corrosion arising from lignosulfonate decomposed residue, interactions which
925 reduce the effectiveness of other additives at temperature over 400 ° F (204 °C) (Meister et
926 al., 1985). Chang et al. (2019) synthesized a novel filtration loss reducer by grafting AM and
927 AMPS on to nano-lignosulfonate (LS). The incorporation of the amide group in the polymer
928 backbone allows the graft polymer to absorb onto clay particles. In addition, the sulfonic acid
929 group in the AMPS monomer attracts electrons from the –OH because of to the S – O – π
930 bonds producing conjugation, thereby improving the ability to resist high salinities and high
931 calcium concentration. The filtration behaviour of the graft polymer was evaluated by hot
932 rolling a WBM at 392 ° F (200 °C) for 16 h. It was observed that the graft-LS containing drilling
933 fluid showed a significant reduction in filtration loss volume (7.5 ml).

934 **Discussion**

935 **ROP**

936 Our analysis of the literature on ROP clearly shows that the key to increasing ROP is to
937 decrease the viscosity and the density of the drilling fluid with the caveat that good hole
938 cleaning must be maintained. For this a low density thermally stable shear thinning fluid is
939 required.

940 Literature research reveals that the most successful method of reducing mud viscosity and
941 density is to use a foamed fluid (Quintero, 2002; Al-Darweesh, 2022). These fluids also offer
942 strong shear thinning behaviour. However, the use of foams is operationally complex and the
943 foams themselves have limited stability especially at higher temperatures (Harris and

944 Reidenbach, 1987; Negrao, 1999; Li et al, 2014; Saxema *et al*, 2014; Verma et al, 2017). A
945 promising alternative technology is the use of colloidal gas aphron (CGA) (Molaei and Waters,
946 2015; Alizadeh and Khomehchi, 2019; Padasar et al, 2020). CGAs are essentially *stabilised*
947 microfoams (Save and Pangarkar 1994). Aphron-based drilling fluids have been successfully
948 deployed in several field operations (Belkin et al, 2005). For example, CGA drilling fluids have
949 been shown to offer an effective solution to lost circulation problems in multiple oilfield
950 applications, particularly when underbalanced drilling is preferred. For example, it is reported
951 that CGA based drilling fluids were successfully employed in mature low-pressure reservoirs
952 of Lake Maracaibo. Over 90% of fluid recovery and excellent hole cleaning properties were
953 reported (Ramirez *et al.*, 2002; Montilva *et al.*, 2002). CGAs in combination with calcium
954 carbonate were used with similar success in depleted North Sea formations, where the fluid
955 was used to seal the existing perforations during the first phase of the project (White *et al.*,
956 2003). The authors also emphasised the attractiveness of CGA fluids in that they do not
957 require compressors, high-pressure hoses or any other high-cost equipment required for air
958 or foam drilling.

959 CGA fluids consist of many colloidally dispersed stable microbubbles most of which have a
960 particle size of 10-100 μm , with the bigger ones reaching 200 μm . The aphron bubbles consist
961 of a spherical core of air and a protective multilayer film. High stability, elasticity and good
962 strength of the film enables aphrons to form a stable drilling fluid (Belkin et al, 2005).
963 Furthermore, CGAs show favourable rheological properties. They have high viscosity at low
964 shear rates allowing for efficient hole cleaning and carrying of the cuttings, whilst they are
965 highly shear thinning (Khomehchi et al., 2016; Bjorndalen et al., 2008).

966 Three main components are required for CGA production – water, viscosifier and foaming
967 agent (surfactant). Xanthan gum has been the polymer of choice for most CGA applications
968 because of its high availability and low cost. However, as discussed above xanthan gum is
969 thermally unstable for temperatures above 130 °C, so developing high temperature stable of
970 CGAs is a current focus area (for example, Zhu et al, 2021). Improved thermal stability can be
971 achieved by using polymers that have a high thermal stability and/or through the use of solid
972 stabilisers and viscosifiers. Indeed, solids can replace surfactants in stabilising foams and CGAs
973 (Yang et al., 2019) should molecular surfactants prove to be insufficiently thermally stable as
974 well.

975 **Polymers**

976 *Biopolymers*

977 It is clear that unmodified biopolymers have an intrinsic thermal stability limit introduced by
978 the presence of the acetal group in the molecule's backbone. For the unprotected acetal
979 group, present in most biopolymers, this limit is of the order of 90 °C. Natural modifications
980 of the molecule which provides some protection of the acetal groups, as present in
981 scleroglucan, can increase the thermal stability of the molecule, although not dramatically so,
982 achieving a stability of ca. 135 °C in the case of scleroglucan. Functionalisation of the
983 biopolymers and the formation of composite with minerals and inorganic materials can raise
984 the thermal stability of the polymer. However, this can be both expensive and difficult to

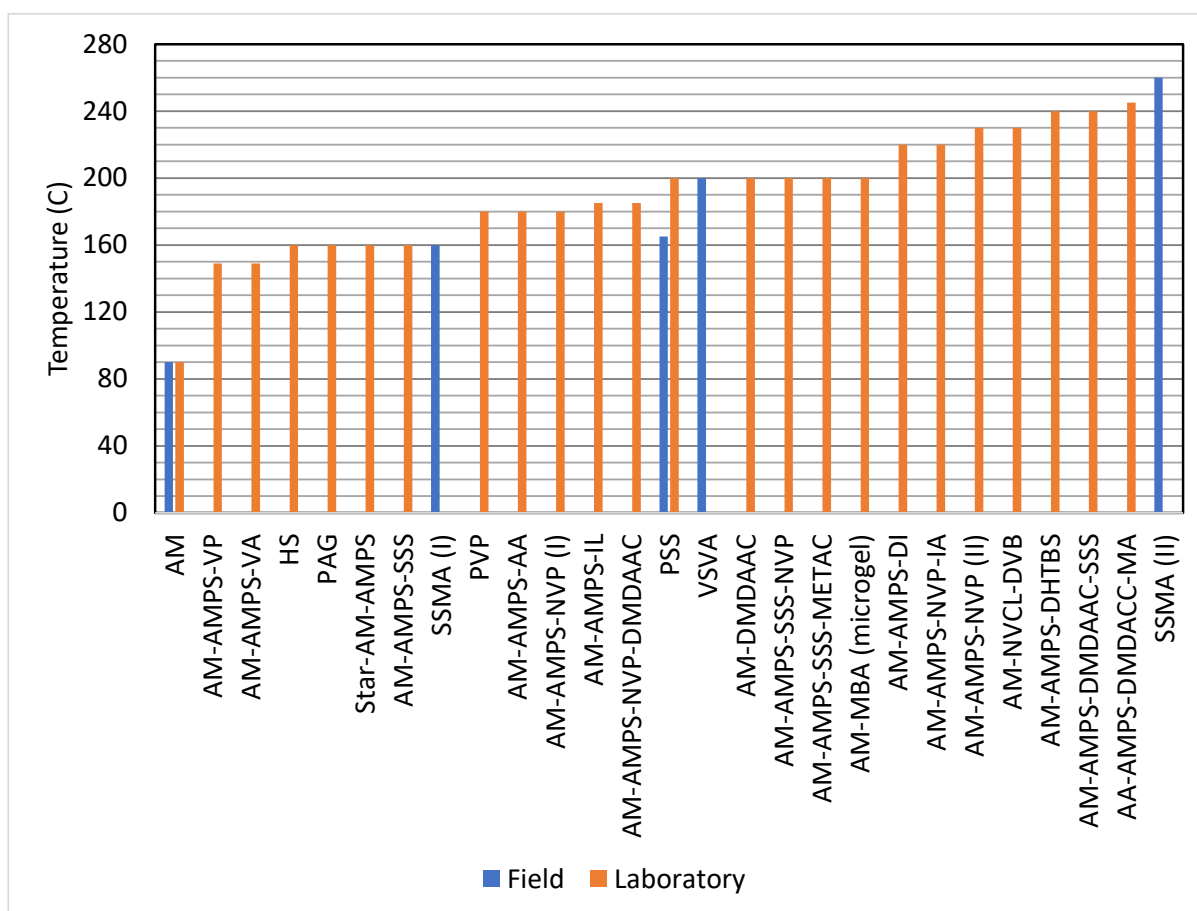
985 achieve. Such materials do not appear to be commercially available and moreover, the
986 benefits in thermal stability are unclear – they have not been tested at temperatures relevant
987 to geothermal drilling.

988 *Synthetic polymers*

989 The data collated above has been plotted as a bar chart of maximum tested temperature at
990 which the formulated drilling fluid exhibits thermal stability (note that the tests used, and
991 success criteria vary with each study) against the polymer class employed (Figure 4).

992

993



994

995

996 **Figure 4. Thermal stability of different classes of polymer identified in the literature (field**
997 **and laboratory measurements). See Table 1 for the definition of the monomers displayed.**
998 **Excludes Thermal Gravimetric Analysis data.**

999 From Figure 3 it is clear that very few of the synthetic polymers suggested for drilling fluid
1000 formulations have actually been tested in the field, the vast majority of studies being
1001 laboratory studies. Moreover, the laboratory studies do not usually cover all of the properties
1002 and duties of drilling fluids so provide a limited picture of thermal stability. Nevertheless, it
1003 is clear that synthetic polymers can offer thermal stability advantages over biopolymers

1004 although the base polymer (polyacrylamide) that forms the backbone of most water-soluble
1005 polymers also has a relatively low thermal stability, again of the order of 90 °C (although there
1006 is some laboratory data claiming stability up to 150 °C). The data clearly shows that in order
1007 to be stable at geothermal drilling temperatures, polyacrylamide must be co-polymerised
1008 with other monomers that protect the backbone. An alternative to this is make polymers that
1009 do not include acrylamide monomers. However, both solutions introduce increased cost in
1010 manufacturing the polymer (the more co-monomers there are, the higher the cost). This is
1011 clearly shown by the data supplied in Davoodi et al (2023a, 2023b) where only sodium styrene
1012 sulfonate has a lower unit cost than acrylamide (AM) and diallyl dimethyl ammonium chloride
1013 DMDAAC) is some 25-35 times more expensive than acrylamide. The most commonly
1014 employed co-monomer, 2-acrylamido-2-methyl-propanesulfonic acid (AMPS), is ca. twice as
1015 expensive as acrylamide.

1016 It is also clear from Figure 1 that the maximum thermal stability that has been achieved is
1017 ~260 °C, which whilst a considerable improvement over biopolymer-based fluids, still leaves
1018 a large window of geothermal drilling operations inaccessible to polymer-based fluids. Given
1019 the wide range of monomers employed in making the disclosed polymers and the complex
1020 molecular architectures employed, it is unclear at present how this maximum temperature
1021 can be exceeded. Given that two different versions of the same polymer (e.g., SSMA and AM-
1022 AMPS-NVP) can have dramatically different thermal stabilities, the ratio of monomers in the
1023 polymer backbone, the functional group proximity, and the blockiness of the polymer (e.g.
1024 AABBBCC versus AAABBBCCC, ABCABC or ACCABB etc) must play an important part in the
1025 thermal stability. We are not aware of a systematic study of this for a given polymer type.
1026 The desired physical properties of hydrolytically thermally stable polymers should be
1027 amenable to study by computational chemistry (both atomistic and coarser grained
1028 simulations could shed light on the structure-function relationship) which, if combined with
1029 a systematic synthetic programme and simplified high throughput testing, could allow the
1030 development of novel high stability polymers. In addition, a systematic data set would be
1031 amenable to study using the machine learning methods outlined by Davoodi et al. (2023c)
1032 allowing a predictive model for the rheological properties of different polymer architecture
1033 to be predicted.

1034 Finally, it is unclear how many of the advanced polymers are available commercially in the
1035 quantities needed for drilling, especially given the potential high cost of these materials.

1036 As with biopolymers, thermal stability can be increased by forming a polymer-inorganic solid
1037 composite. Whilst clay-based composites use relatively cheap materials, other more complex
1038 composites do not. Currently these materials do not appear to be commercially available.

1039 *Solids*

1040 The use of solids to improve the rheological properties of drilling fluids and to improve fluid
1041 loss behaviour is an attractive option. Indeed, thermal stabilities exceeding the best synthetic
1042 polymers can be achieved (290 °C). Relatively cheap clay minerals and inorganic solids can
1043 offer advantages over polymers. Even simple nanoparticles can improve drilling fluid

1044 performance and thermal stability whilst having the advantage of being commercially
1045 available in large quantities.

1046 **Conclusions**

- 1047 1. Current key parameters governing RoP are still considered to be the 8 parameters
1048 used in the Bourgoyne-Young regression model.
 - 1049 a. Many ML models based on the B&Y model have recently emerged for RoP
1050 prediction, but they do not include detailed drilling fluid properties – non-
1051 Newtonian rheology at HT, filtration (filtercake thickness / permeability),
1052 formation damage, etc.
- 1053 2. RoP depends on the rheology / composition of the drilling fluid.
- 1054 3. RoP increases linearly with decreasing PV, solid content, and mud weight for both
1055 sedimentary and geothermal rock formations.
- 1056 4. Biopolymers are not suitable for high temperature geothermal drilling (> 130°C)
- 1057 5. Modified biopolymers and biopolymer composites may be effective above the
1058 stability limit for biopolymers alone; however, the cost of these systems will be higher
1059 and are not currently readily available.
- 1060 6. Simple polyacrylamide-based drilling fluids are not recommended for high
1061 temperature geothermal operations. Modified and alternative synthetic polymers can
1062 have high thermal stability and have been demonstrated to withstand the
1063 temperatures encountered in part of the geothermal drilling window. However, the
1064 cost of these materials will be high and commercial availability is uncertain.
- 1065 7. Synthetic polymer-inorganic material composites have been shown to improve
1066 synthetic polymers thermal stability. However, the limits on this are not known. Such
1067 materials are not currently commercially available.
- 1068 8. Solid additives offer the potential to improve drilling fluid properties under
1069 geothermal drilling conditions. Furthermore, relatively cheap materials such as
1070 sepiolite and palygorskite can be employed. Nanoparticles offer an intriguing
1071 opportunity to modify and control drilling fluid behaviour at high temperatures using
1072 commercially available materials.

1073 **Recommendations**

- 1074 1. The use of biopolymers in high temperature geothermal drilling operations is not
1075 recommended.
 - 1076 2. Low-PV, low-solid content, and low-mud-weight drilling fluid formulations need to be
1077 developed to enhance RoP. The literature suggests that potential solutions include:
 - 1078 i. Foams
 - 1079 ii. Aphrons
- 1080 These systems should employ HT stable polymers, particle-stabilisation, and particle
1081 composites (nanocomposites).
- 1082 3. Solid additives to improve drilling fluid properties under HT geothermal drilling
1083 conditions should be investigated, especially to further develop low-PV fluids.

- 1084 i. It is recommended to further explore the use of solids to provide
1085 drilling fluid functionality under geothermal conditions.
1086 ii. Nanoparticle application in drilling fluids should be explored further.
1087 4. A systematic study of the effect of copolymer architecture for a range of high
1088 performing monomers (AMPS, NVP etc) should be carried out to determine the
1089 controls on hydrolytic thermal stability. Both computational and experimental studies
1090 should be able to help elucidate the optimal structure-function relationships.
1091 5. Polymer-solid composites should be investigated especially with the aim of improving
1092 upper thermal limits of geothermal drilling fluids.
1093 6. Modified bio-polymer systems should be investigated to determine if it is feasible and
1094 cost-effective to extend organic polymer functionality to high temperatures.

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1098 **Author Contributions**

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