



PROJECT MESOWAS

A solar-based membrane reactor for hydrogen production

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Introduction: The MESOWAS project

Membrane-based solar thermal cycles for the synthesis of green hydrogen

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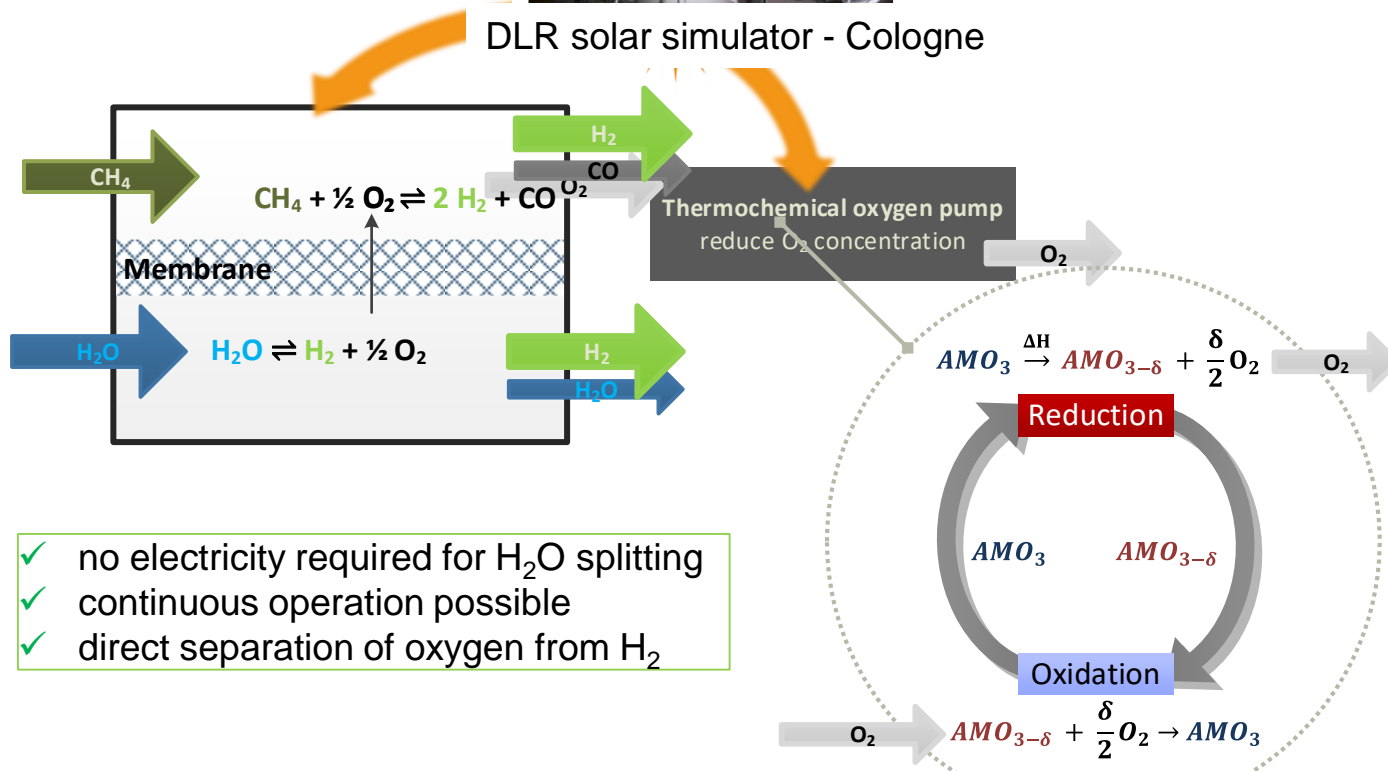
Federal Ministry of Education and Research

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DLR solar simulator - Cologne

- Option A:** Sweep gas or thermochemical O₂ pump
- Option B:** Partial oxidation of biomethane or biogas



- ✓ no electricity required for H₂O splitting
- ✓ continuous operation possible
- ✓ direct separation of oxygen from H₂

Aim of project:

1. Experimental proof-of-concept of a solar membrane reactor for water splitting
2. Development of membrane
3. Investigation of different approaches to reduce the oxygen concentration on permeate side
4. Potential analysis of membrane technology

Start 01.08.2022

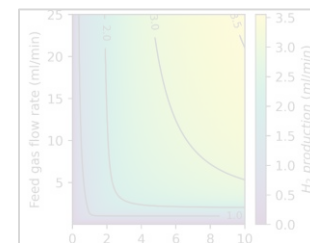
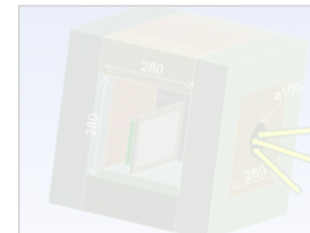
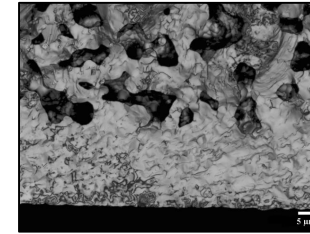
End 31.07.2025

Consortium:

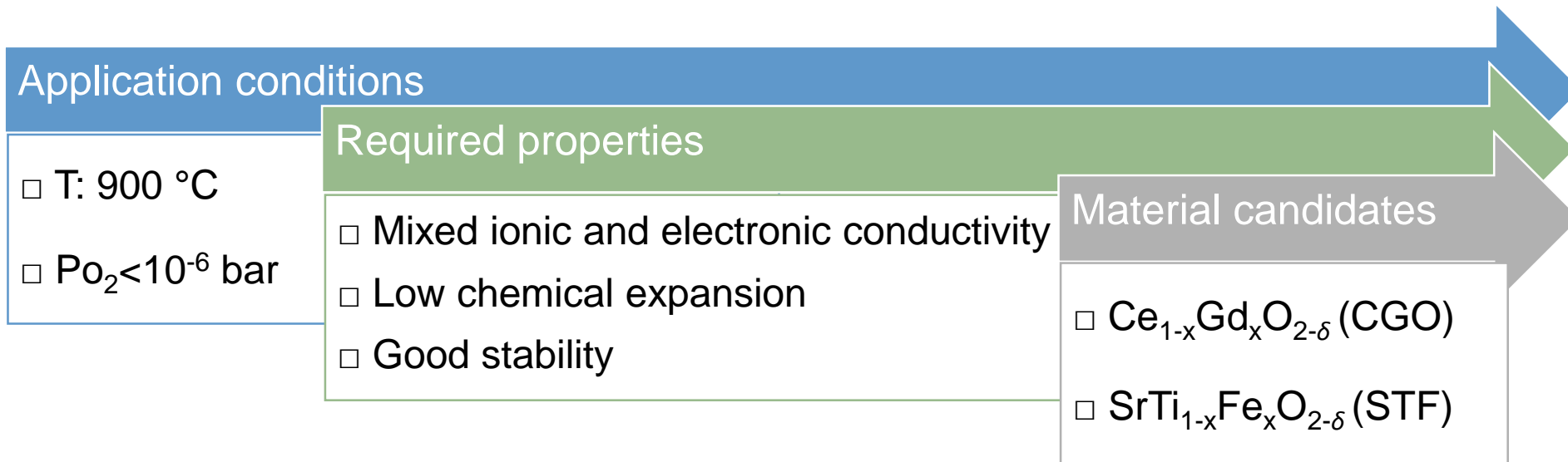


Agenda

1. Material selection and membrane fabrication
2. Membrane reactor development
3. Solar energy integration
4. Reactor modelling



Material selection



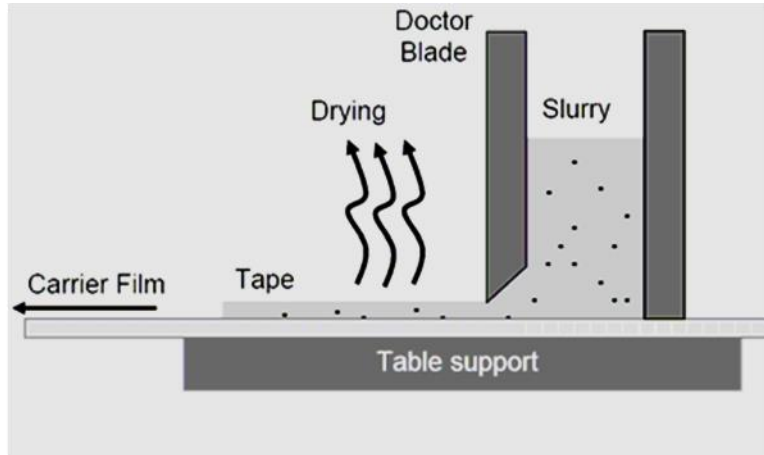
- Lower chemical expansion from Ti^{4+} (0.605 nm) to Ti^{3+} (0.67 nm) for STF compared to Ce^{4+} (0.97nm) to Ce^{3+} (1.143nm) in CGO
- 25 mol% Fe doping ensure applicable conductivity and structural integrity under low P_{O_2}

→ STF material doped with 25 mol% Fe is selected

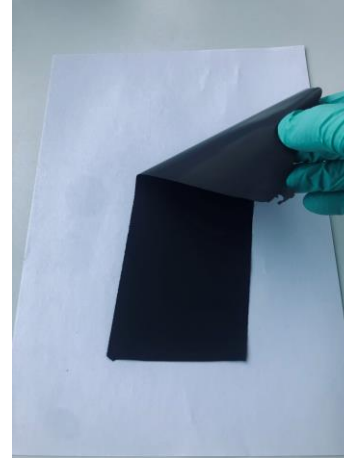
Membrane fabrication and performance



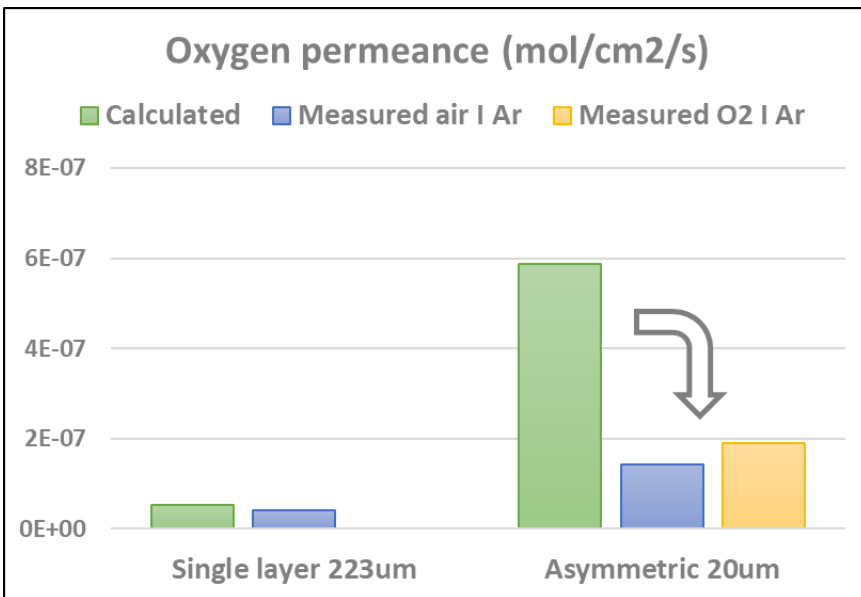
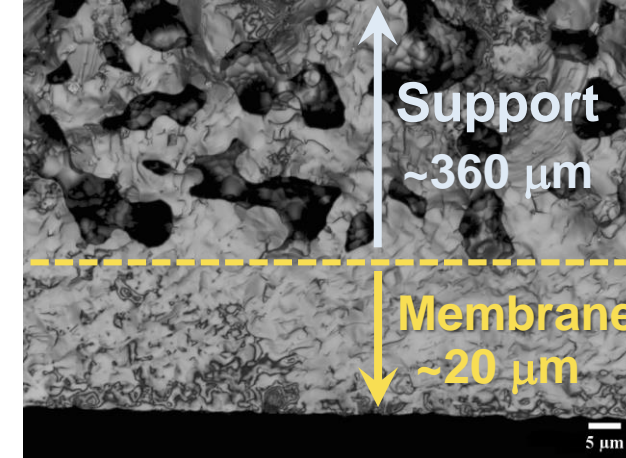
Tape Casting



Green Tape



Sintered asymmetric membrane



Bulk transport control:

$$\text{Oxygen Permeance} = - \frac{j_{O_2}}{\int_{P'_{O_2}}^{P''_{O_2}} d \ln P_{O_2}} = \frac{R}{16F^2} \cdot \frac{1}{L} \cdot \sigma_{amb} \cdot T$$

- **Single layer membrane:** the measured value \approx calculated value, validating the assumption of bulk transport control
- **Asymmetric membrane:** the measured value \leq calculated value, indicating limiting surface exchange and gas diffusion through the porous support \rightarrow catalysts required

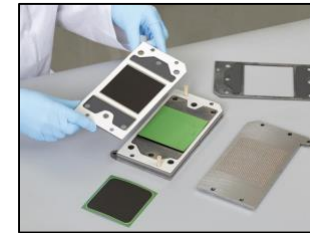
Agenda



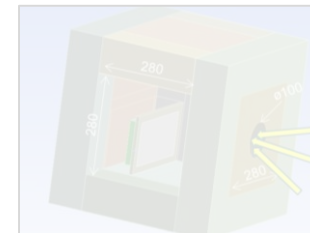
1. Material selection and membrane fabrication



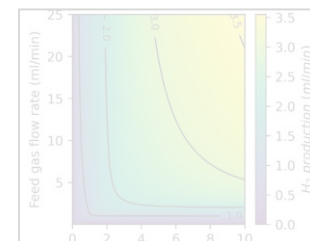
2. Membrane reactor development



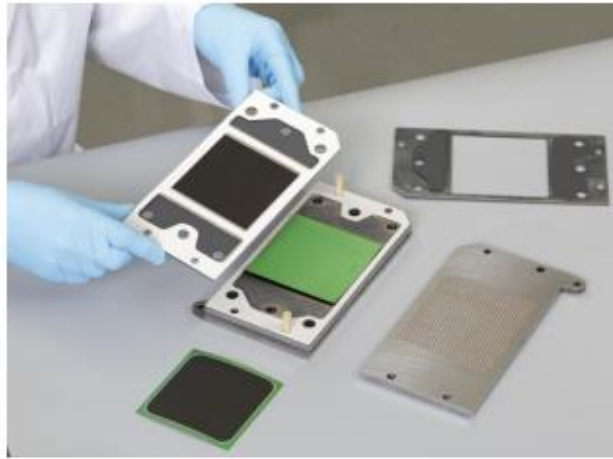
3. Solar energy integration



4. Reactor modelling



Reactor design: From F10 Jülich Solid Oxide Electrolysis design to a membrane reactor



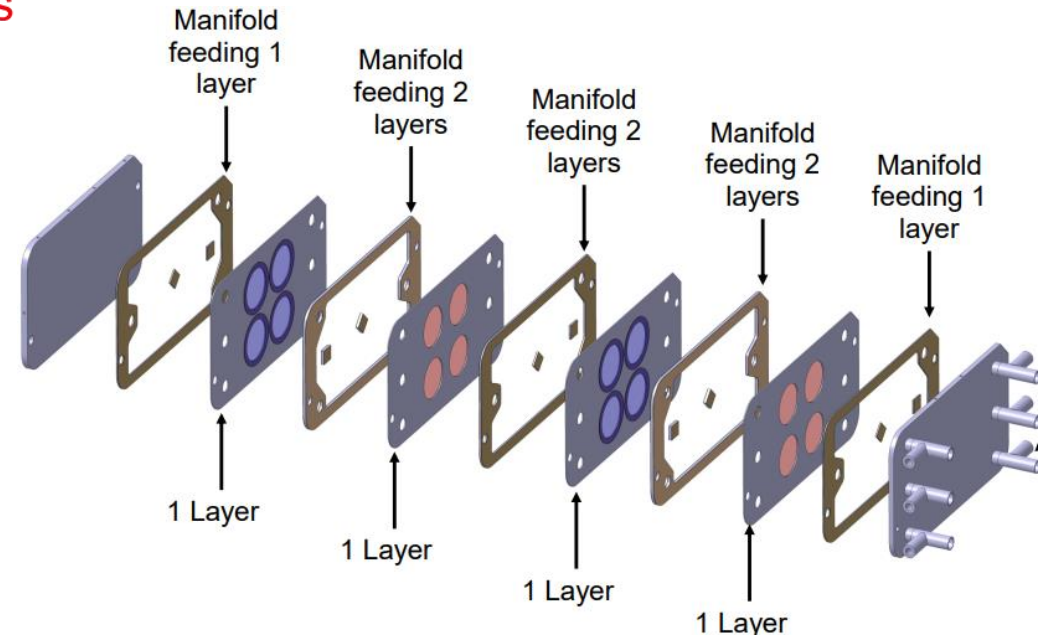
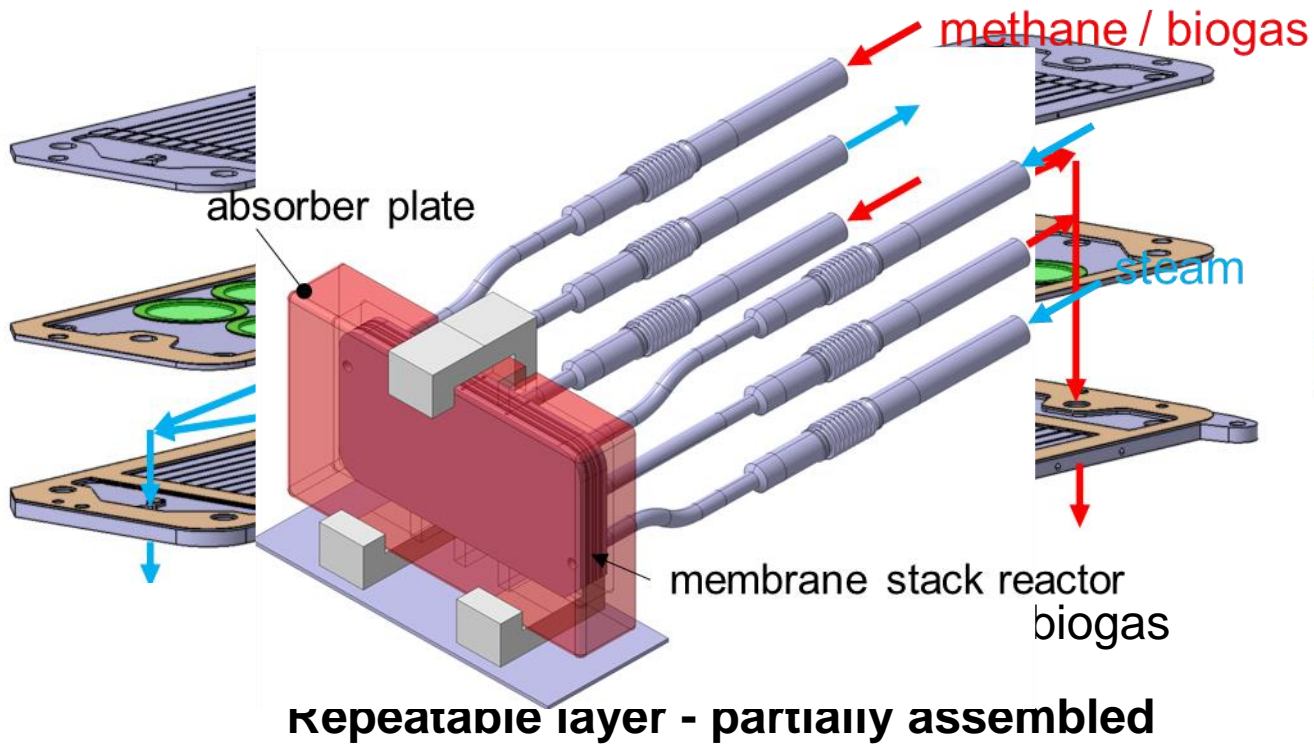
SOC „F10“

Feasibility of the design:

- Similar outer envelope can be used; X layer stack footprint: 220 mm x 120 mm **x scalable**
- Different membrane shapes can be adapted (e.g. circular or rectangular)
- Shape and type of glass solders can be adapted to membrane and metals of the design
- Stacks allow scalability of system

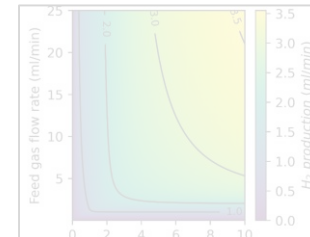
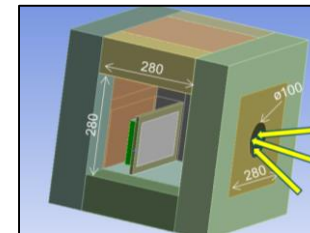
Design of membrane reactor

proof-of-concept of the solar membrane reactor (using stacks):



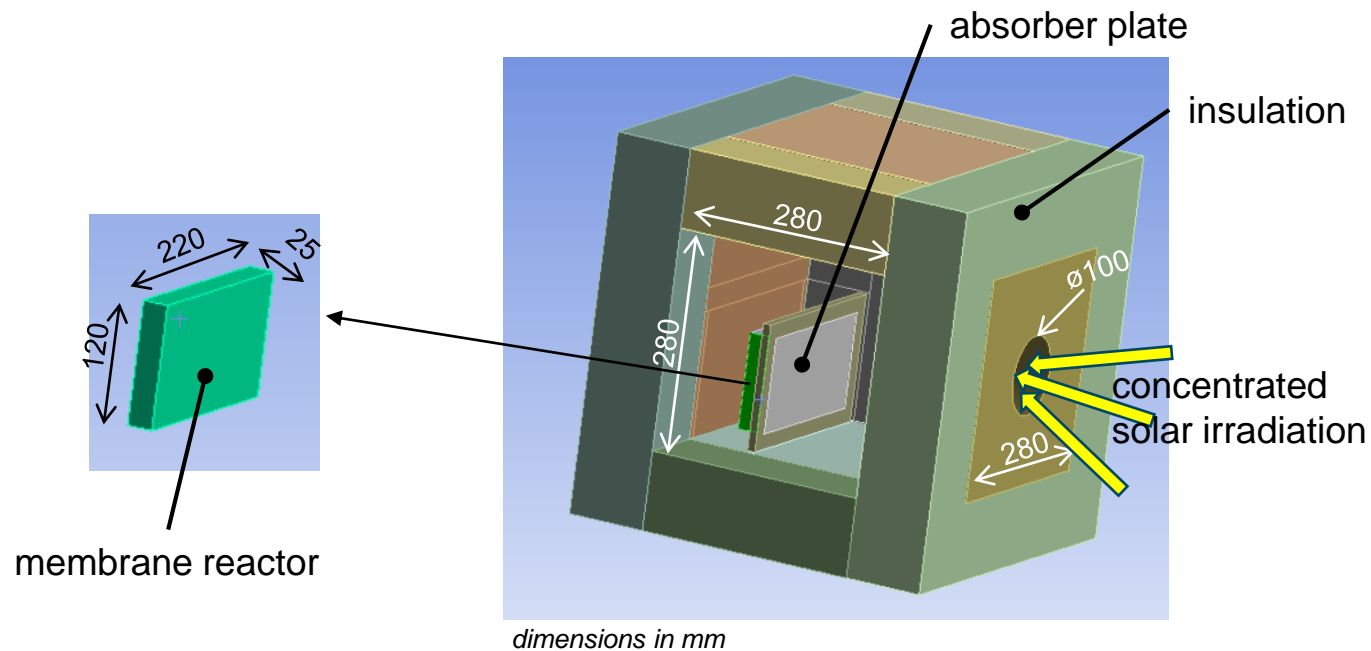
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Solar energy integration

- Membrane reactor stack inside an open insulation „box“
- Concentrated solar energy enters cavity and hits the absorber plate in front of the stack



Integration of solar energy

Using intermediate Heat Transfer Fluid
(scale up concept analysis)

**Using indirect irradiation of stack
(experiments)**

**Homogeneous T distribution on
membrane reactor**

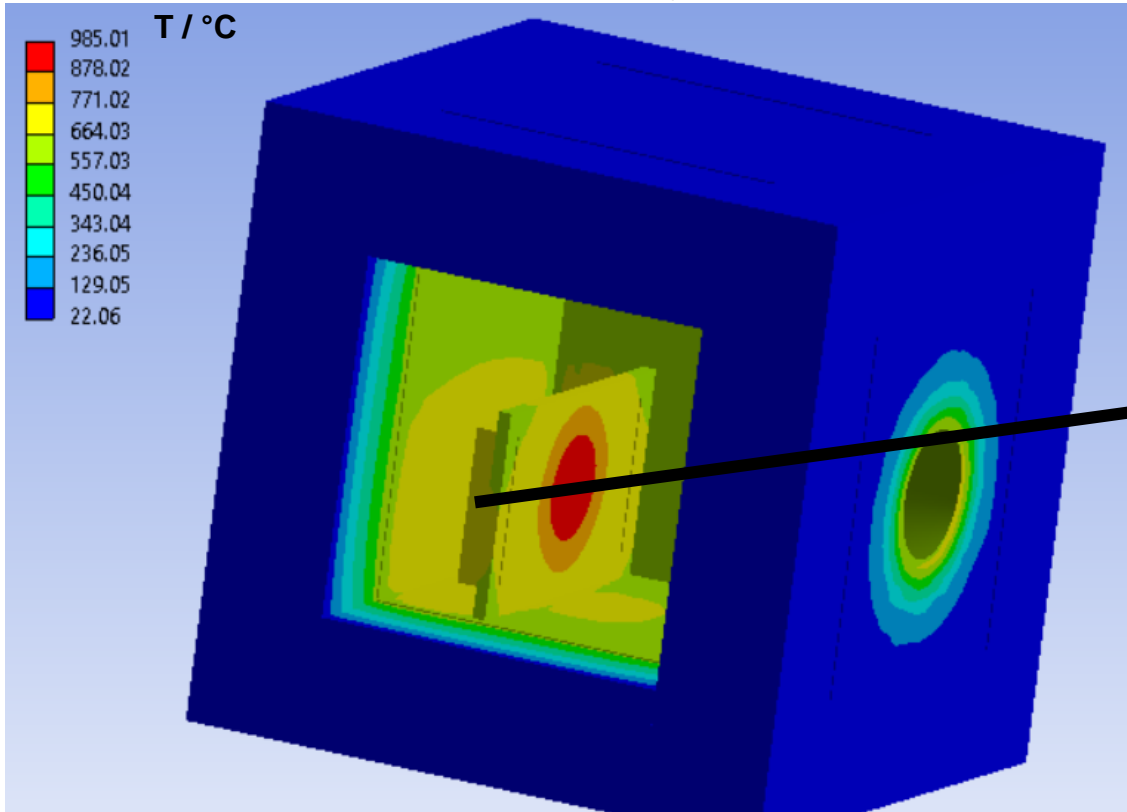
- Temperature for experiments:
(800 – 900 °C)
- Max. allowable T gradient: **50 K**

Simulations of solar flux distribution on membrane reactor

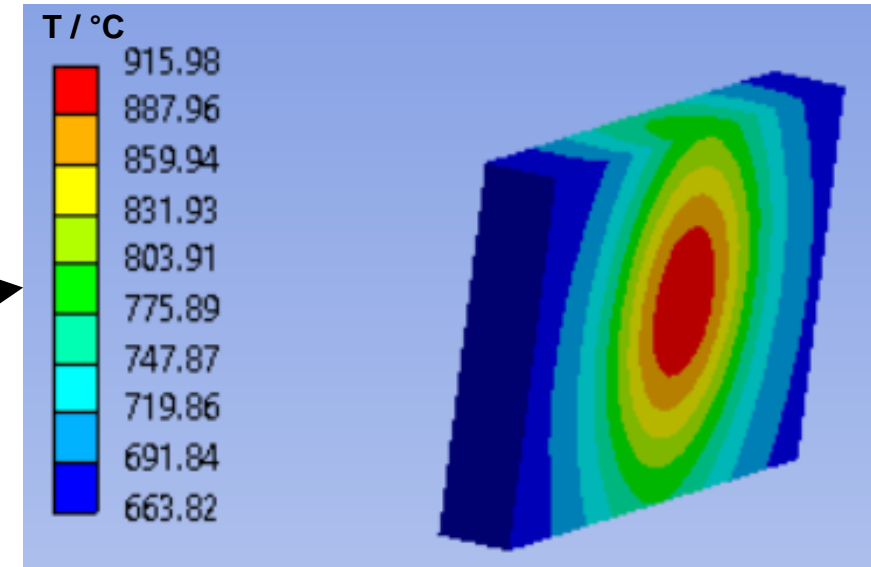
Material of irradiated plate: steel



T distribution of cavity



T distribution membrane reactor

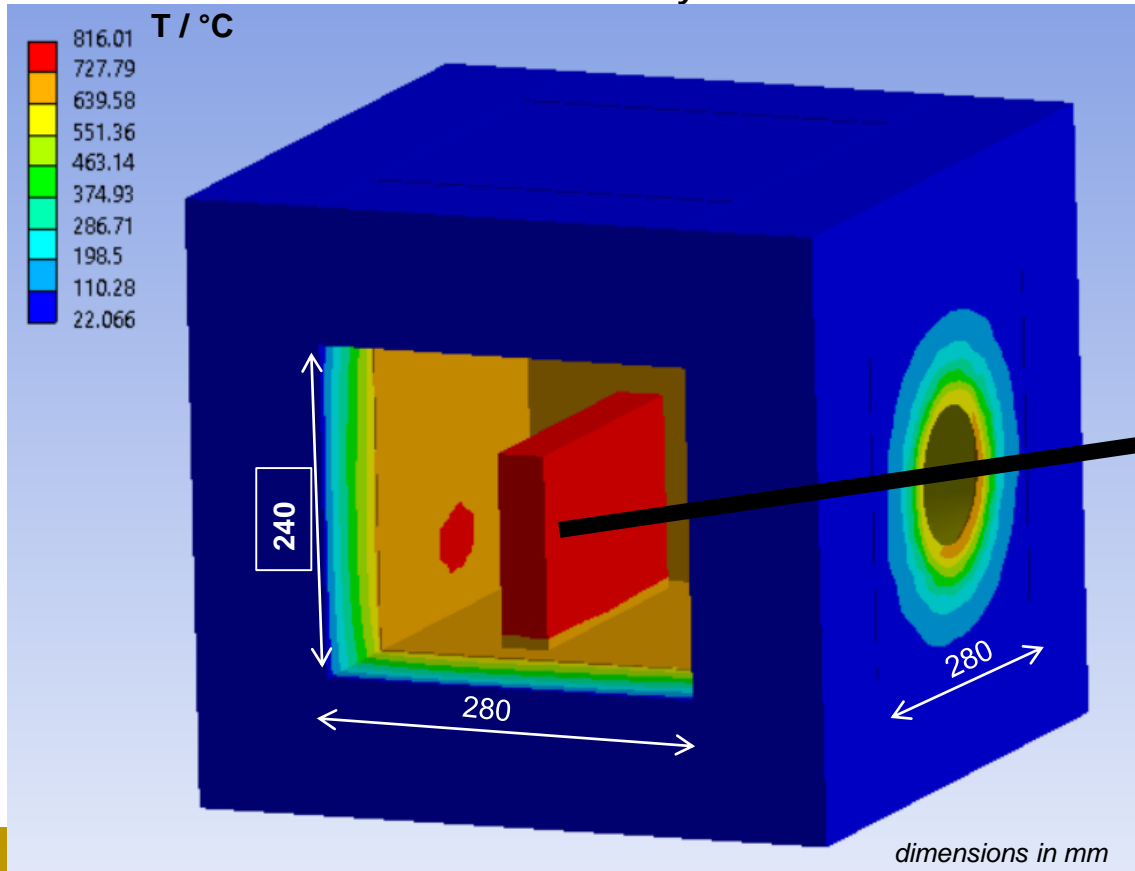


irradiated plate: steel

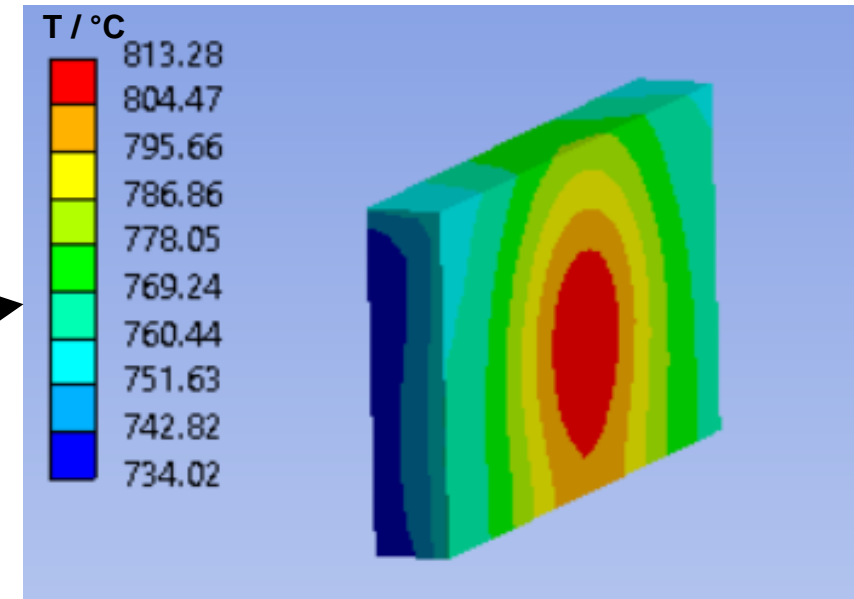
- Hot spot in central part → temperature gradient too large!

Modification of volume of cavity to reach higher temperatures

T distribution of cavity



T distribution membrane reactor

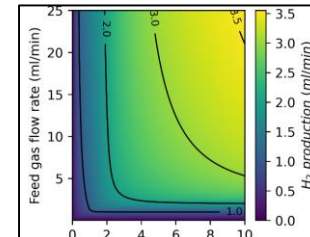
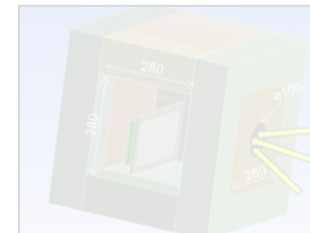


irradiated plate: copper

- High temperature achieved, but T gradient still > 50 K

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0D – Reactor Modelling

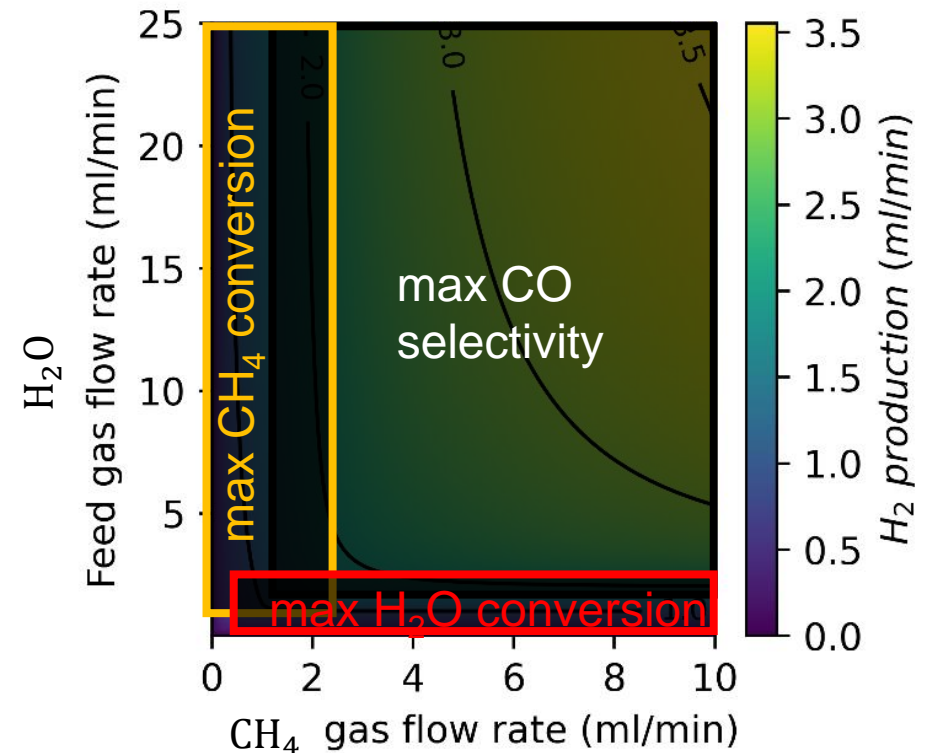
- Development of a 0D model for initial design iterations [1]

Assumptions:

- Chemical equilibrium on both sides
- Infinite fast diffusion in gas phase
- Isothermal

Implementation:

- Coupling of two Gibbs minimization problems by Wagner equation



H_2 production for 1 cm^2 active membrane area

3D – Reactor Modelling

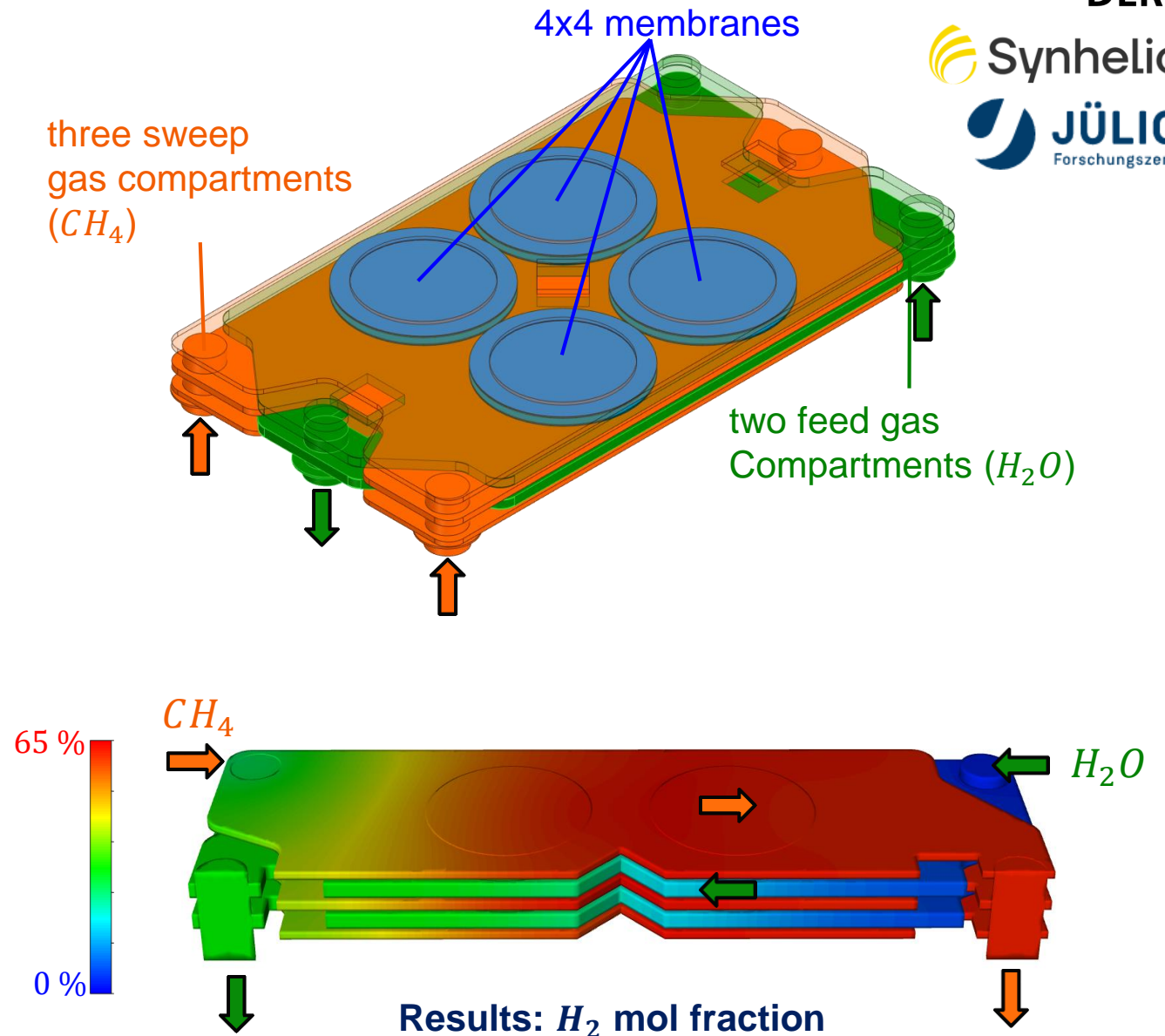
- Development of a 3D model to investigate geometrical effects

Assumptions:

- Chemical Equilibrium at the membrane surface

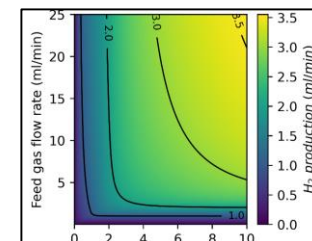
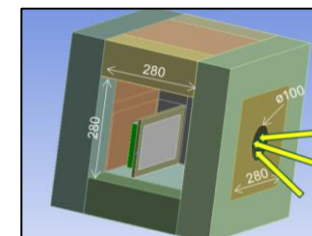
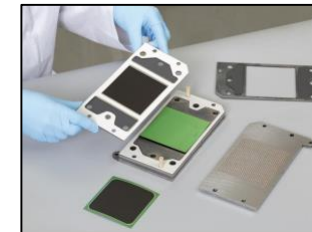
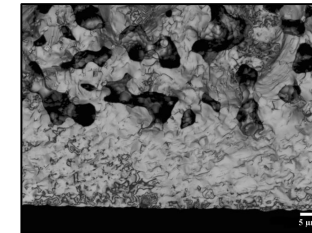
Implementation:

- Fluid flow equations are solved using Ansys Fluent
- Surface reactions and oxygen permeation are modelled using User Defined Functions



Conclusion

- STF-based membranes with 25 mol% Fe showed best mix of low thermal expansion and ambipolar conductivity for 800 °C – 900 °C and low pO_2 operation.
- Design of a first-of-a-kind solar membrane stack reactor.
- Solar energy can cover the energy demand of the reactor, but homogenisation of flux distribution still ongoing.
- 0D and 3D reactor model to identify suitable operation parameters.



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