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DFT Investigation of CH4 and H2O Adsorption on Pd (111), Ni (111), Pt (111), and Ir(111) Surfaces

Abdulrauf Onimisi Ibrahim^{1,2*}, Baba Jibril El-Yakubu²

- ¹ Department of Chemical Engineering, Universiti Malaya, Kuala Lumpur, MALAYSIA
- ² Department of Chemical Engineering, Ahmadu Bello University, Zaria, NIGERIA

*Corresponding Author: s2003719@siswa.um.edu.my DOI: https://doi.org/10.30880/jst.2023.15.02.008

Article Info

Abstract

Received: 11 October 2023	Using density functional theory (DFT) calculations, the surface Gibbs
Accepted: 10 December 2023	free energy of methane and water adsorption on Pt(111), Ir(111),
Available online: 13 December 2023	Ni(111), and Pd(111) surfaces was investigated. DFT computations
	were employed to investigate the adsorption of methane and water
	molecules on unit cells with varying coverage levels of 0.11, 0.25, 0.50
Keywords	and 1.00 monolayors and the aggregation of $H_{2}O$ over clean transition
Water methane transitional metals	and 1.00 monolayers and the aggregation of h20 over clean transition
vale, includie, transitional metals,	metal surfaces. The adsorption configuration was assessed to
adsorption	experimental findings to evaluate our computational approaches'
	accuracy and reliability. A thermodynamic diagram was constructed for
	exploring the adsorption of CH4 and H2O on metal surfaces. The order
	of the methane adsorption energies on different metal surfaces is as
	follows: $Pd(111) > Pt(111) > Ni(111) > Ir(111)$. A more significant
	number of H_2O molecules on the transition metal surfaces reduces the
	contact between the metal surfaces and water molecules during water
	contact between the metal surfaces and water molecules during water
	aggregation. The thermouynamic stability of water and methane
	adsorption coverage was found to be best on the Pt(111) surface.

1. Introduction

The commercial significance of the catalytic breakdown of CH₄ on metallic surfaces is remarkable [1]. CH₄ is a primary constituent of natural gas and plays a remarkable role in hydrogen generation. The primary methods utilised in the production of hydrogen include methane steam reforming (SRM) [CH₄ + H₂O \rightarrow + 3H₂+ CO] [2], partial oxidation of methane [CH₄ + $\frac{1}{2}$ O₂ \rightarrow 2H₂ + CO] [3], and methane dry reforming [CO₂ + CH₄ \rightarrow CO + 2H₂] [4]. The SRM is the process by which CH₄ and H₂O react over a nickel catalyst, accounting for nearly 98% world's supply of hydrogen gas[5]. To get a high conversion of methane, it is necessary to employ a reactor operating at elevated temperatures ranging from 700°C to 1,000°C [6]. This is due to the fact that the process involving methane is entirely endothermic. The utilisation of optimal catalysts is imperative within the industrial sector to enhance the efficiency of methane steam reforming. Furthermore, the comprehension of catalytic reactions can be achieved through the application of quantum chemistry principles [7].

Water and methane adsorption on transition metal surfaces have been the attention of numerous studies. Many articles have confirmed that the single water molecule favours adsorbing at the atop site on metal surfaces [8-10]. Pache et al. [11] conducted a study to examine the water adsorption process on a clean Ni(111) surface, spanning from low to saturation coverage. The researchers observed a desorption peak within the temperature range of 438-443°C. This peak can be attributed to water molecules in the 1st monolayer and the hydrogen bonding interactions among these water molecules. Additionally, the adsorption energy of a single water

© 2023 UTHM Publisher. All rights reserved. This is an open access article under the CC BY-NC-SA 4.0 license. molecule was determined to be 0.44 eV. Chen et al. [12] examined the physisorption of CH_4 on Pt(111) through reflection absorption infrared spectroscopy. The researchers discovered that the desorption energy of CH_4 on the Pt(111) surface was measured to be 18.3 kJ/mol at a surface temperature of 305 °C.

The application of DFT inside a thermodynamic model allows for predicting the preferred coverages on the surface of a catalyst, considering the influence of intensive state variables. In this work, we utilised periodic DFT calculations to investigate the impact of H₂O and CH₄ adsorption on the surfaces of Pt(111), Ni(111), Ir(111), and Pd(111). The calculations were performed using gradient-corrected (PW91) functionals. Thermodynamic phase diagrams employ surface Gibbs free energies (SGF) to determine the optimal adsorbate coverage on a catalyst surface, considering gas phase temperature and pressure variations.

2. Materials and Methods

2.1 Energy Calculations

Periodic DFT calculations were executed with Dmol³ of Materials Studio 8.0 [13] to analyse geometries and electronic energies at 0 K. The correlation and exchange functional were defined by generalised gradient approximation (GGA) using PW91 functional [14]in conjunction with a doubled numerical basis set plus polarisation [15]. Brillouin-zone integrations were carried out using $4 \times 4 \times 1$, $5 \times 5 \times 1$, $10 \times 5 \times 1$ and $10 \times 10 \times 1 \text{ k-point grid for p(3×3), p(2×2), p(1×2) and p(1×1)surface, respectively. A value of 0.005 Ha was adapted for thermal smearing to obtain accurate electronic convergence. Conditions for convergence comprised a lower limit of <math>1.0 \times 10^{-5}$ Ha for energy, 5.0×10^{-3} Å⁻¹ for maximum displacement and 2.0×10^{-3} Å⁻¹ for maximum force, and with self-consistent field convergence of 1.0×10^{-6} Ha. The lattice constants of Ni, Pt, Pd, and Ir were determined to be 3.53550Å, 3.98950Å, 3.96340Å, and 3.8926Å, respectively. These values closely matched the experimental results of 3.52Å [16], 3.916Å [17], 3.89Å [18] and 3.84Å [17] respectively.

The metal (111) surfaces were simulated using a four-layered slab, with only the top two layers relaxed while the bulk optimal structure was imposed on the other levels. The unit cell employed for the adsorption of methane and water is reproduced in all three dimensions, resulting in an endless surface with a vacuum thickness of 15 Å. Two methodologies were employed to examine the consequences of coverage. Initially, the unit cell size is manipulated while maintaining constant adsorbates. Secondly, by increasing the quantity of adsorbates within the unit cell. The initial methodology was employed to investigate the impact of methane coverage. The investigation involved the examination of methane at various coverages by the process of adsorbing a single methane molecule on unit cells with dimensions of (3×3) , (2×2) , (2×1) , and (1×1) . The selection of several surface sizes, namely $p(3\times3)$, $p(2\times2)$, $p(1\times2)$, and $p(1\times1)$, was made to accurately reproduce the distinct coverage levels of 0.11, 0.25, 0.50, and 1.00 monolayer, respectively. Figure 1 depicts the several adsorption sites on the metal (111) surface, including atop, bridge, fcc, and hcp. The determination of adsorption energy involved calculating the energy released per methane/water molecule adsorbed on the clean surface, as described by equation 1.

$$E_{ads} = E_{methane/M} - (E_M + E_{methane}) \qquad (1)$$



Fig. 1 Side and top views of Ir(111) surface showing coverage of 0.11 (3x3), 0.25 (2x2), 0.50 (2x1) and 1.00 (1x1) monolayer

The variable $\mathbf{E}_{methane}$ is the slab energy of the metal surface with methane molecule adsorbed on it. \mathbf{E}_{M} is the slab energy of the metal surface in the absence of the adsorbed molecules, and $\mathbf{E}_{methane}$ is the electronic



energy of methane. This implies that the more negative \mathbb{E}_{ads} , the stronger the interactions between the metal surface and the adsorbed species [8].

The activation energy of the reactions was determined by calculating the transition states (TS) employing linear synchronous transit and quadratic synchronous transit techniques. For the reaction, $CD \rightarrow C + D$ on X(111) catalyst, activation energy (E_A) and reaction energy (ΔE) were determined using equations 2 and 3.

$$E_A = E_{TS/X} - E_{(C+D)/X}$$
 (2)

$$\Delta E = E_{(C+D)/X} - E_{CD/X} \qquad (3)$$

The slab energy of TS is denoted by $E_{TS/X}$, the slab energy of the catalyst surface with adsorbed C and D species is denoted by $E_{(C+D)/X}$, and the slab energy of the catalyst surface with adsorbed CD species is denoted by $E_{CD/X}$.

2.2 Aggregation of H₂O on Metal Surface

For H₂O aggregation on the metal (111) surface with a (2x2) unit cell, the formation energy ($E_{formation}$) of (H₂O)_n cluster on M(111) surface comprises two types of interactions; one is the interaction between the metal surface and (H₂O)_n cluster; the other is within the adsorbed (H₂O)_n molecules. The formation energy ($E_{formation}$) is expressed in equation (4):

$$E_{formation} = \frac{\left[E_{(H_2O)_n/M} - (E_M + nE_{H_2O})\right]}{n}$$
(4)

Where E_M is slab energy of clean metal surface, $E_{H_2O_m}/M$ is slab energy for the metal surface with the adsorbed $(H_2O)_n$ cluster, *n* is number of H_2O molecule in $(H_2O)_n$ cluster, and E_{H_2O} is energy of H_2O molecule. The following methods are used to calculate the adsorption energy (E_{ads}^o) and hydrogen-bond interaction (E_H) of $(H_2O)_n$ system:

$$E_{H} = \frac{\left[nE_{(H_{2}0)_{n}} - nE_{H_{2}0}\right]}{n}$$
(5)

$$E_{adg}^{e} = E_{form} - E_{H}$$
(6)

Where $E_{(H_{2}O)_{n}}$ is (H₂O)_n cluster single point energy.

2.3 Thermodynamic Calculations

The catalytic methane steam reforming reaction typically occurs at high temperatures between 650°C to 900°C [19]. For these conditions, density functional theory can yield entropies of elementary reaction steps using statistical thermodynamics and calculated electronic energy. The SGF energy (Γ) was used to assess the most reliable surface coverage, which is a function of the gas phase condition. Γ was determined from the Gibbs energy with vibrational frequencies contribution is calculated as shown in equation 7.

$$\Gamma(\mathbf{T}, \mathbf{p}_i) = \frac{G_{ads}(T) - n_M G_{bulk}(T) - \sum_i n_i G_{m,gas,i}(\mathbf{T}, \mathbf{p}_i)}{2 \times SA}$$
(7)

With G_{bulk} and G_{ads} is the Gibbs free energy of the bulk metal atom and the adsorbate coverage, respectively. SA is the unit cell surface area. n_i and n_M represent the total number of adsorbed molecules and the total number of metal atoms in the unit cell.

3. Results and Discussion

3.1 CH₄ Adsorption on Metal Surface at Different Coverage

Multiple positioning of the CH₄ molecule were investigated at all adsorption sites on the transition metal (111) surface, as depicted in Figure 1. Table 1 presents a summary of the height of methane from the metal surface (h_{M-c}), the bond length between hydrogen atoms and carbon atom (d_{C-H}), and the adsorption energies (E_{ads}) for various coverage levels of 1.00, 0.50, 0.25, and 0.11 monolayer (ML).



0.11 ML 0.25 ML 0.50 ML 1.00 ML Metal Adsorption d_{C-H} d_{C-H} E_{ads} E_{ads} h_{M-C} h_{M-C} h_{M-C} h_{M-C} Surface Site dc-н (Å) Eads (kJ/mol) dc-н(Å) Eads (kJ/mol) (Å) (Å) (Å) (Å) (Å) (Å) (kJ/mol) (kJ/mol) -10.38 1.105 -10.99 1.102 3.58 1.106 3.56 3.61 54.81 3.69 1.094 148.90 atop 3.82 1.098 bridge 3.86 1.099 -9.07 3.82 1.100 -9.93 55.91 3.84 1.092 149.32 Pt(111) fcc 3.81 1.099 -8.76 3.85 1.099 -9.82 3.83 1.098 56.00 3.82 1.092 149.71 -9.68 1.098 3.75 1.100 -8.60 3.79 1.100 3.82 56.04 3.81 1.091 149.76 hcp 3.43 -12.28 3.59 1.094 38.26 157.45 atop 1.106 3.56 1.104 -13.16 3.47 1.096 bridge 1.102 3.62 1.093 39.09 158.00 3.51 1.102 -10.373.54 -11.64 3.69 1.094 Pd(111) 158.45 3.50 -10.383.62 1.093 62.10 1.094 1.102 3.54 1.102 -11.16 3.63 fcc 3.50 1.102 -10.43 3.57 1.101 -11.36 3.60 1.100 62.07 3.68 1.093 158.44 hcp 48.22 atop 3.80 1.101 -10.083.95 1.099 -11.05 3.91 1.091 3.91 1.091 184.44 4.12 1.097 -9.18 3.90 1.098 -9.88 4.20 1.095 71.68 3.90 1.089 185.02 bridge Ir(111) fcc 4.24 1.097 -9.07 3.89 1.098 -9.45 4.22 1.095 71.69 4.19 1.089 185.02 185.03 71.77 4.20 1.097 -9.15 4.01 1.097 -10.13 4.22 1.096 3.91 1.089 hcp 115.77 382.62 3.91 1.098 -10.33 4.13 1.098 -12.51 3.89 1.088 3.72 1.092 atop 3.95 3.62 1.090 382.84 bridge 1.098 -10.18 4.08 1.098 -12.13 116.52 3.72 1.093 Ni(111) 3.97 -10.02 1.098 -12.09 1.090 116.44 3.74 1.092 382.88 fcc 1.098 4.04 3.59 4.02 -10.02 -11.52 3.80 1.087 116.22 3.75 1.092 382.87 hcp 1.098 3.81 1.100

 Table 1 - Methane adsorption on metal (111) surface

The favoured adsorption site for methane is the atop site on all metal surfaces, consistent with findings from earlier studies [20, 21]. At surface coverages of 0.50 and 1.00 monolayer on the metal surfaces, the adsorption energy of CH₄ exhibited a positive value, indicating that the adsorption process was thermodynamically unstable. The adsorption energies of CH₄ on the Pt(111) surface were found to be -10.99 kJ/mol and -10.38 kJ/mol for coverages of 0.25 and 0.11 ML, respectively, indicating their high stability. This finding is consistent with the previous research conducted by Gautier et al. [22] (-9.7 kJ/mol). The favoured adsorption site for methane on Pd(111) is the atop site, exhibiting adsorption energies of -12.28 kJ/mol and -13.16 kJ/mol at coverages of 0.25 and 0.11 monolayer, respectively. These values closely align with the experimental findings of -17.02 kJ/mol [23]. The preferred adsorption site for methane on Ni(111) is the atop site, exhibiting an adsorption energy of -10.33 kJ/mol 0.11 monolayer, which is in agreement with the experimental findings (Ni in carbon nanotube) [24] having an adsorption energy of -8.51 kJ/mol. According to the data presented in Table 1, it can be observed that methane exhibits the most pronounced interactions with the Pd(111) surface. The interaction between CH₄ and metal surfaces exhibits an evident weakness, suggesting physisorption. This observation aligns with previous studies on the physisorption of CH₄ on several metal surfaces, including Rh(111) [25], Pd (100) [26], etc.



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3.2 CH₄ Dissociation on Metal Surface

In this section, the dissociative process of CH_4 into $CH_3 + H$ was investigated at the coverage of 0.11 ML. The initial state, TS and final state structures are illustrated in Figure 2.



Fig. 2 Reactant, TS and product structures for $CH_4 \rightarrow CH_3 + H$ reaction on Ir(111) surface



Fig. 3 The energy profiles of CH_4 to CH_3 dissociation on metal (111) surfaces

Based on the data depicted in Figure 3, it is evident that the initial stage entails the adsorption of CH_4 onto the surface. Subsequently, the adsorbed CH_4^* species undergoes dissociation, resulting in the formation of CH_3^* and H^* species. The relative activation energies for the surfaces of Ir(111), Ni(111), Pd(111), and Pt(111) are 92, 114, 127, and 116 kJ/mol. The activation barrier for the dissociation of CH_4 on the Ir(111) surface is consistent



with the values reported by Qiet et al [21], specifically 89.7 kJ/mol at a coverage of 0.25 ML. This finding is also in keeping with experimental results [27] which reported an activation barrier of 106 kJ/mol. Based on the calculation results, it can be concluded that methane dissociation has a higher preference for the Ir(111) surface than other metal surfaces.

3.3 Adsorption of H₂O on M(111) Surface at Different Coverage

The investigation focused on examining various orientations of water adsorption at the atop site. Table 2 presents a summary of the adsorption energies (E_{ads}), the height of water from the metal surface (h_{M-0}) and the bond length between oxygen atom and hydrogen atoms at 1.00, 0.50, 0.25, and 0.11 monolayer. The most favourable adsorption location for H₂O on the Ni(111) surface is the atop position, where the H₂O molecule is oriented parallel to the nickel surface. The adsorption energies of H₂O molecules on a nickel surface (Ni(111)) at different coverages, specifically 1.00, 0.50, 0.25, and 0.11 ML, are recorded as -5.22, -38.19, -42.23, and -44.76 kJ/mol, respectively. The findings align with the empirical evidence presented in a prior investigation., which determined the value to be -42.45 kJ/mol [9]. The distance between the Ni(111) surface and H₂O molecules on Ir(111), Ni(111), Pd(111), and Pt(111) surfaces, with a coverage of 0.11 monolayers (ML), are -58.04, -46.07, -45.81, and -44.76 kJ/mol, respectively. The water molecule exhibits the most pronounced interactions with the Ir(111) surface.

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Motol Advantion			0.11 ML			0.25 ML		
Surface	site	h_{M-O}	d_{O-H}	E_{ads}	h_{M-O}	d_{O-H}	E_{ads}	
Surface	site	(Å)	(Å)	(kJ/mol)	(Å)	(Å)	(kJ/mol)	
Pt(111)	atop	2.44	0.977	-45.81	2.53	0.977	-42.53	
Pd(111)	atop	2.43	0.976	-45.76	2.53	0.977	-42.53	
Ir(111)	atop	2.34	0.979	-58.04	2.38	0.981	-54.43	
Ni(111)	atop	2.21	0.978	-44.76	2.29	0.979	-42.23	
Matal	Adaption		0.50 N	/L		1.00 N	ΛL	_
Surface	site	h_{M-O}	do-н	E_{ads}	h_{M-0}	о <i>do-н</i>	E_{ads}	
Surface	site	(Å)	(Å)	(kJ/mol)	(Å)	(Å)	(kJ/mol)	-
Pt(111)	atop	2.76	0.985	-53.68	3.28	8 0.978	-46.07	
Pd(111)	atop	2.66	0.985	-55.72	3.18	8 0.981	-46.55	
Ir(111)	atop	2.57	0.987	-58.45	3.30	0.982	-43.00	
Ni(111)	atop	2.73	1.007	-38.19	3.2	0.985	-5.22	

 Table 2 H₂O adsorption on metal (111) surface

3.4 Aggregation of H₂O on Metal Surface

The most stable water adsorption configurations were identified using a stepwise adsorption energy analysis [9]. The strength of hydrogen bond interaction within the $(H_2O)_n$ cluster is directly proportional to the magnitude of the negative hydrogen-bond interaction (E_H) . The more negative Eads, the stronger the interaction of $(H_2O)_n$ cluster with the metal surface [8]. The most stable arrangements of H_2O clusters on the metal surfaces are shown in Figure 4. Table 3 displays the E_H , formation energy, and adsorption energy of the $(H_2O)_n$ cluster on metal surfaces. The findings of this study indicate that a rise in the quantity of aggregate water molecules leads to an increased hydrogen-bond interaction among these molecules. Consequently, the interaction between water and metal surfaces weakens, aligning with the findings of Hao et al. [8]. The interaction between water molecules was found to be strongest on the Ir (111) surface, while the Ni(111) surface exhibited the smallest interaction.

Ir(111) surface			Pt(111) surface			
(H2O)n	E_{form}	E_H	E ^e ads	E_{form}	E_H	
	(KJ/MOL)	(KJ/MOL)	(KJ/MOL)	(KJ/MOL)	(KJ/MOL)	(KJ/MOI)
1	-54.43	0.00	-54.43	-42.53	0.00	-42.53
2	-62.81	-13.71	-49.10	-55.71	-13.71	-42.00
3	-71.43	-29.83	-41.60	-66.23	-29.83	-36.40
4	-70.46	-37.40	-33.07	-64.75	-37.40	-27.35

 Table 3 H₂O aggregation on metal (111) surface



	Pd(111) surface				Ni(111) surface			
(H ₂ O) _n	E_{form}	E_H	E_{ads}^c	Eform	E_H	E_{ads}^c		
	(kJ/mol)	(kJ/mol)	(kJ/mol)	(kJ/mol)	(kJ/mol)	(kJ/mol)		
1	-43.72	0.00	-43.72	-42.16	0.00	-42.16		
2	-56.54	-13.71	-42.83	-52.94	-13.71	-39.22		
3	-65.05	-29.83	-35.22	-57.65	-29.83	-27.82		
4	-69.17	-37.40	-31.77	-61.10	-37.40	-23.70		







Fig. 4 Adsorption of most stable water aggregation configurations on(a) Ir(111) (b) Ni(111) (c) Pd(111) (d) Pt(111) surfaces

3.5 Thermodynamics

In accordance with equation 7, we employed the parameter Γ as a benchmark to evaluate the stability of the adsorbed system of H₂O and CH₄ under various conditions. It was observed that a greater negative value of Γ corresponded to a higher degree of stability in the adsorbed structure [28]. Figure 5 illustrates the relationship between the surface free Gibbs energy of the adsorbate, specifically H₂O and CH₄, and temperature at a pressure of 1 bar for each respective surface.





Fig. 5 SGF energies as a function of temperature at 1 bar for H₂O and CH₄ adsorption on Ir(111), Ni(111), Pd(111) and Pt(111) surface

The experimental findings indicated that the surface-free Gibbs energy associated with the adsorption of methane and water on the metal surface exhibited positive values when the coverage reached 0.50 and 1.00 monolayers (ML). The surface-free Gibbs energy exhibited a negative value at coverage levels of 0.25 and 0.11 ML on the metal surfaces. The thermodynamically most stable coverage for water and methane adsorption at all adsorbate coverages was found to be the Pt(111) surface. The order of stability for water and methane



adsorption on various surfaces, rated from highest to lowest, is as follows: Pt(1 1 1), Pd(1 1 1), Ir(1 1 1), and Ni(111).

4. Conclusion

This study explores the adsorption of CH_4 and H_2O on Pt(111), Ni(111), Ir(111), and Pd(111) surfaces at varying coverages and adsorption sites. Additionally, the aggregation of H_2O on these metal surfaces is examined through the utilisation of DFT calculations.

The preferred adsorption site for methane on the metal surface is located at the top position. The thermodynamic stability of methane adsorption on metal surfaces was determined to be unstable at coverage levels of 0.50 and 1.00 monolayers (ML), whereas it was found to be stable at coverage levels of 0.25 and 0.11 ML. The order of decreasing activation energies for the dissociation of CH_4 to CH_3 on various surfaces is as follows: Pd(111) > Pt(111) > Ir(111).

In the context of H_2O adsorption on metal surfaces, a reduction in water coverage on the surface leads to a corresponding decrease in the height of the water layer above the metal surface. An increase in the adsorption energy accompanies this decrease in coverage. The number of H_2O molecules present influences the aggregation of H_2O on metal surfaces. An increase in the quantity of H_2O molecules leads to a greater interaction of hydrogen bonds among the water molecules. Consequently, this decreases the interaction between the H_2O molecules and the metal surfaces. The thermal stability of methane and water on different surfaces can be ranked in descending order as follows: Pt(111) > Pd(111) > Ir(111) > Ni(111).

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Conflict of Interest

Authors declare that there is no conflict of interests regarding the publication of the paper.

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