

# STEAM SYSTEM ASSESSMENT TOOL (SSAT): OVERVIEW

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## **New Steam Tool: Steam System Assessment Tool (SSAT)**

Purpose: Software tool to evaluate every aspect of a complicated or simple steam cycle.

A Department of Energy certified steam system heat balance. The result will be a standardized opportunity analyses for each plant surveyed.

## **SSAT Can Evaluate These Key Steam Improvement Opportunities**

Real Cost of Steam	Condensate Recovery
Steam Quality	Steam Trap Operating Efficiency
Boiler Efficiency	Heat Recovery
Alternative Fuels	Flash Steam Recovery
Cogeneration Opportunities	Steam Leaks
Steam Turbines vs PRVs	Insulation Efficiency
Boiler Blowdown	Emissions Calculations

## **SSAT Can be Used in Two Ways**

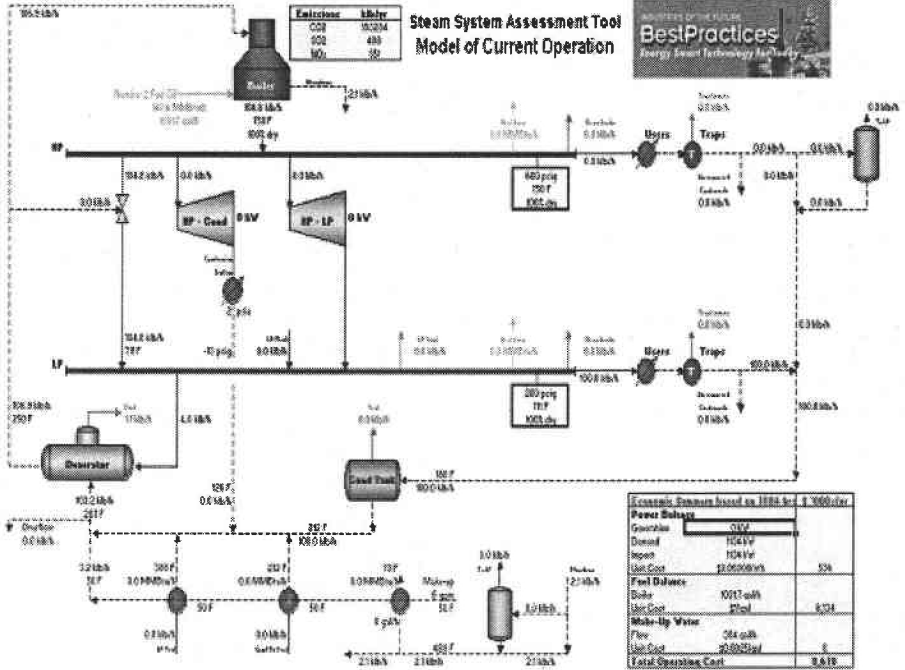
- (1) Information about the existing system is entered into the program and 18 different projects can be exercised to evaluate the impact on the existing plant.
- (2) If the desired improvement is not one of the 18 available projects the system can be modeled twice and the results compared.

## The 18 Projects in SSAT

Change in steam demand	HP to condensing steam turbine
Use an alternative fuel	Feedwater heat recovery exchanger on condensate vent
Change boiler efficiency	Feedwater heat recovery exchanger on continuous blowdown
Change boiler blowdown rate	Condensate recovery
Blowdown flash to LP header	Condensate flash to MP header
Change steam pressure	Condensate flash to LP header
HP to LP steam turbine	Steam trap losses
HP to MP steam turbine	Steam leaks
MP to LP steam turbine	Improved insulation

### Key SSAT Features

- Choice of 1, 2, or 3 header pressure models
- Schematics of model steam system
- Estimates of site environmental emissions
- Major equipment simulated:
  - boiler
  - back pressure turbines
  - condensing turbine
  - deaerator
  - steam traps, leaks, insulation losses
  - pressure reducing valves
  - flash vessels
  - feedwater preheat exchangers



## Driving Force

What is the main driving force for improving a steam system?  
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- Energy
- Reliability
- Maintenance
- Productivity
- Quality
- Cost avoidance
- Emissions reductions

## Measure

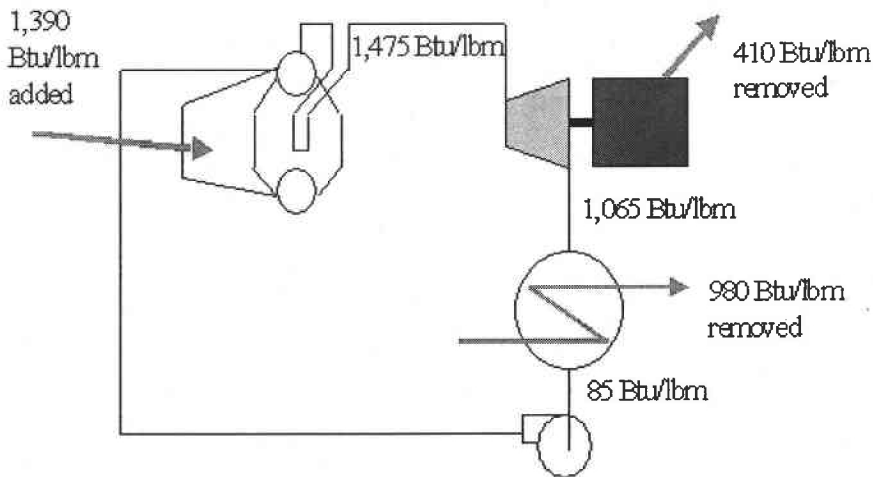
You are not managing what you do not measure.

- steam flow, total steam generated
- fuel used, cost of fuel
- electricity used, electricity cost
- flue gas oxygen (excess combustion air)
- makeup water used

### New Dry Kiln Systems

- For a new system, an evaluation should be made of generating steam at high pressure with superheat, reducing the steam pressure to the dry kilns through a steam turbine generator, and using the exhaust steam to dry lumber.
- This cycle would provide the facility with all of its electricity requirements and all of its steam for drying lumber.
- The above system will provide the faculty with the lowest possible energy costs.

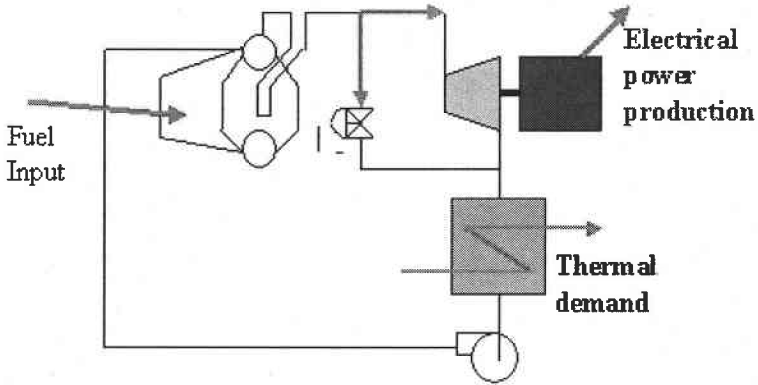
### Utility Power Cycle



$$\eta = \frac{\dot{W}_{electrical}}{\dot{E}_{fuel}} = \frac{410 \frac{Btu}{lbm}}{1,390 \frac{Btu}{lbm}} = 30\%$$

## Industrial Power Cycle

Steam generated at high pressure and temperature.  
Steam pressure reduced through turbine generator.  
Exhaust steam used to dry lumber.



## Improving Existing Dry Kiln Systems

### Reduce stack losses

- reduce excess combustion air
- economizers, air heaters

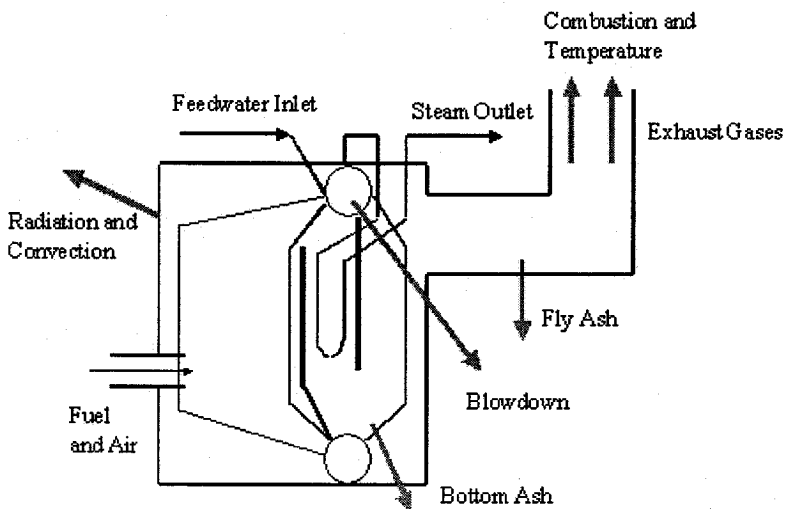
### Reduce blowdown losses

- reduce makeup water
- improve makeup water quality
- install blowdown heat recovery

### Recover Energy in Distribution System

- recover more condensate
- recover sensible heat in the condensate
- improve steam trap maintenance
- improve insulation

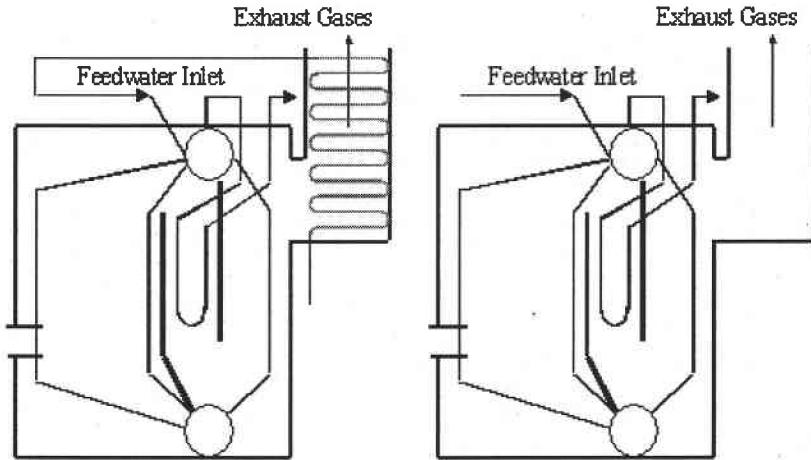
# Identify Boiler Losses



Typical Green Wood Stack Loss [%]

Flue Gas O <sub>2</sub> Content [%]	Flue Gas Temperature - Combustion Air Temperature [°F]																		
	230	250	270	290	310	330	350	370	390	410	430	450	470	490	510				
1.0	21.5	21.9	22.3	22.7	23.1	23.5	23.9	24.3	24.7	25.1	25.5	25.9	26.3	26.7	27.2				
2.0	21.7	22.1	22.5	22.9	23.4	23.8	24.2	24.6	25.1	25.5	25.9	26.3	26.8	27.2	27.6				
3.0	21.9	22.4	22.8	23.2	23.7	24.1	24.6	25.0	25.5	25.9	26.4	26.8	27.3	27.7	28.2				
4.0	22.2	22.6	23.1	23.6	24.0	24.5	25.0	25.4	25.9	26.4	26.8	27.3	27.8	28.3	28.7				
5.0	22.5	23.0	23.4	23.9	24.4	24.9	25.4	25.9	26.4	26.9	27.4	27.9	28.4	28.9	29.4				
6.0	22.8	23.3	23.8	24.4	24.9	25.4	25.9	26.4	27.0	27.5	28.0	28.6	29.1	29.6	30.2				
7.0	23.2	23.7	24.3	24.8	25.4	25.9	26.5	27.1	27.6	28.2	28.7	29.3	29.9	30.4	31.0				
8.0	23.6	24.2	24.8	25.4	26.0	26.6	27.2	27.8	28.4	29.0	29.6	30.2	30.8	31.4	32.0				
9.0	24.1	24.8	25.4	26.0	26.7	27.3	27.9	28.6	29.2	29.9	30.5	31.2	31.8	32.5	33.1				
10.0	24.7	25.4	26.1	26.8	27.5	28.2	28.9	29.6	30.3	31.0	31.7	32.4	33.1	33.8	34.5				
11.0	25.4	26.2	26.9	27.7	28.5	29.2	30.0	30.7	31.5	32.3	33.0	33.8	34.6	35.4	36.1				
Flue Gas T [°F]	300	320	340	360	380	400	420	440	460	480	500	520	540	560	580				
Ambient T [°F]	70	70	70	70	70	70	70	70	70	70	70	70	70	70	70				

## Economizer



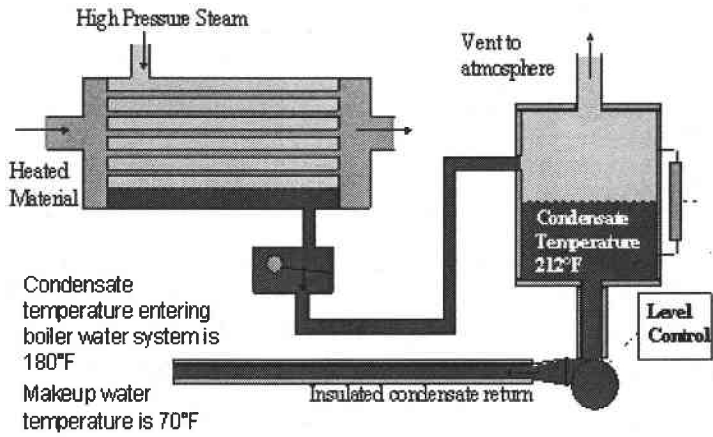
### Steam Distribution Losses

- Steam leaks
- Heat transfer loss through insulation
- Condensate loss
- Overall system

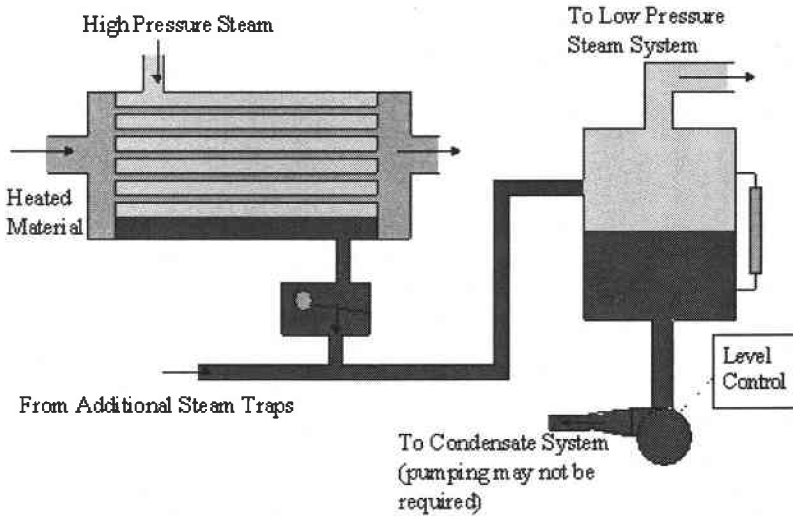
Steam Leaks								
Orifice Diameter [inch]	Leak Rate [lbm/hr]							
	Steam Temperature is 500°F							
	Steam Supply Pressure [psig]							
	50	100	150	200	250	300	350	
1/16	6	10	15	19	24	30	34	
1/8	23	41	59	77	96	119	134	
3/16	51	92	132	173	215	269	302	
1/4	91	163	235	308	382	478	536	
5/16	143	254	367	481	597	747	838	
3/8	206	366	529	693	860	1,075	1,207	
7/16	280	499	720	944	1,170	1,464	1,642	
1/2	366	651	940	1,232	1,528	1,912	2,145	
	20	47	74	100	125	151	176	
Discharge Pressure [psig]								
Discharge coefficient	0.6 dimensionless							

Data based on isentropic compressible flow evaluation

## Condensate Return Example



## Cascade Condensate Systems





## Demonstrating the Usefulness of SSAT

### Three-header system example

- 200, 100, 25 psig
- Wood waste boiler
- 30,000 lbs/hr steam load
- 2,000 kW site electrical load

### Evaluating steam improvements

- Boiler efficiency change
- Boiler blowdown improvements
- Condensate flash to LP
- Reduce steam leaks

## Steam System Assessment Tool

### Stack Loss Calculator

Based on user inputs of Stack Temperature, Ambient Temperature and Stack Oxygen Content, an estimate will be provided of the heat loss from the boiler stack. Losses are expressed as a percentage of the heat fired.

Stack losses are related to SSAT Boiler Efficiency as follows:

$$\text{SSAT Boiler Efficiency} = 100\% - \text{Stack Loss (\%)} - \text{Shell Loss (\%)}$$

Shell Loss refers to the radiant heat loss from the boiler. Typically <1% at full load, 1-2% at reduced load.

### Input Data

Stack Gas Temperature (°F)	550 °F	Stack Temperature - Ambient Temperature = 480°F
Ambient Temperature (°F)	70 °F	

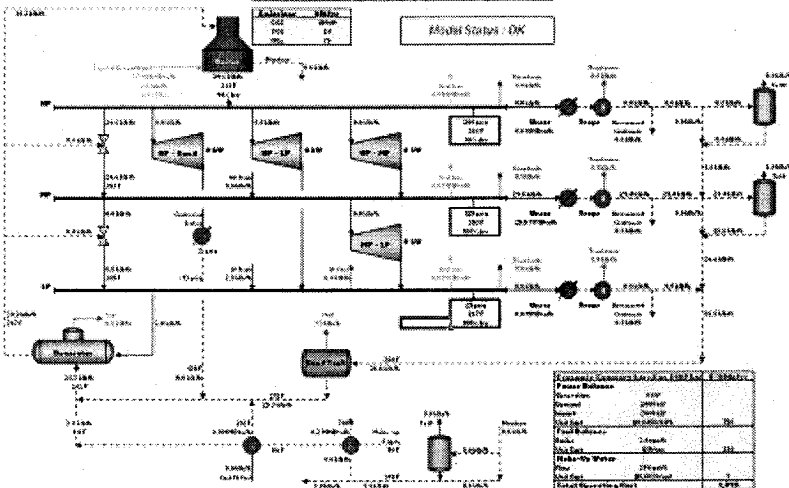
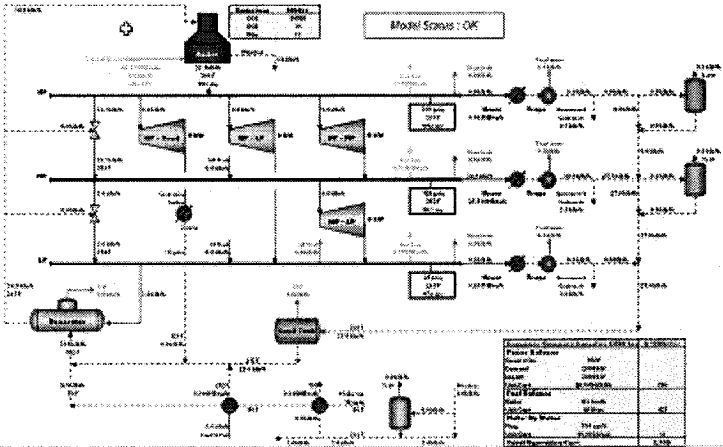
Stack Gas Oxygen Content (%)	10 %
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Note: Stack gas oxygen content is expressed on a molar or volumetric basis

### Results

Estimated Stack Losses for each of the default fuels are as follows:

Natural Gas	28.2 %
Number 2 Fuel Oil	23.5 %
Number 6 Fuel Oil (Low Sulfur)	23.1 %
Number 6 Fuel Oil (High Sulfur)	23.3 %
Typical Eastern Coal (Bituminous)	21.7 %
Typical Western Coal (Subbituminous)	23.2 %
Typical Green Wood	33.5 %



# Steam System Assessment Tool

3 Header Model

## Results Summary

### SSAT Default 3 Header Model

Model Status: OK

Cost Summary (\$ '000s/yr)	Current Operation	After Projects	Reduction
Power Cost	156	156	0 0.0%
Fuel Cost	421	354	68 20.8%
Make-Up Water Cost	35	8	28 43.5%
<b>Total Cost (in \$ '000s/yr)</b>	<b>1,195</b>	<b>1,039</b>	<b>156 13.1%</b>

On-Site Emissions	Current Operation	After Projects	Reduction
CO2 Emissions	50531 Mlb/yr	40649 Mlb/yr	10503 Mlb/yr 20.8%
SOx Emissions	31 Mlb/yr	24 Mlb/yr	6 Mlb/yr 20.8%
NOx Emissions	88 lb/yr	70 Mlb/yr	18 Mlb/yr 20.8%

Power Station Emissions	Reduction After Projects	Total Reduction
CO2 Emissions	6 Mlb/yr	10503 Mlb/yr -
SOx Emissions	6 Mlb/yr	6 Mlb/yr -
NOx Emissions	6 Mlb/yr	15 Mlb/yr -

Note: Calculated based on 10 lbs steam to 1 mwh power input as emissions from a natural gas fired power station. Total reduction values are for site power station.

Utility Balance	Current Operation	After Projects	Reduction
Power Generation	0 kW	0 kW	-
Power Import	2000 kW	2000 kW	0 kW 0.0%
Total Site Electrical Demand	2000 kW	2000 kW	-
Boiler Duty	47.9 MMBtu/h	37.9 MMBtu/h	9.9 MMBtu/h 20.8%
Fuel Type	Typical Green Wood	Typical Green Wood	-
Fuel Consumption	4.6 tons/h	3.6 tons/h	-
Boiler Steam Flow	33.1 Mlb/h	29.6 Mlb/h	3.5 Mlb/h 10.5%
Fuel Cost (in \$/MMBtu)	1.05	1.05	-
Power Cost (as \$/MMBtu)	13.19	13.19	-
Make-Up Water Flow	704 gph	354 gph	349 gph 49.5%

Turbine Performance	Current Operation	After Projects	Marginal Steam Costs
HP to LP steam rate	Not in use	Not in use	(Based on current operation)
HP to MP steam rate	Not in use	Not in use	MP (\$/lb) 1.67
MP to LP steam rate	Not in use	Not in use	MP (\$/lb) 1.69
HP to Condensing steam rate	Not in use	Not in use	LP (\$/lb) 1.58

These values are based on current operation unless otherwise noted.

Customer Management Suite



- List of Selected Projects**
- Increase boiler efficiency
  - Decrease boiler blowdown rate
  - Install blowdown heat exchanger
  - Increase MP condenser recovery
  - Install condensate float to LP
  - Improve pipework insulation

## Fuel Savings or Steam Capacity Increase

- Boiler efficiency is equal to the energy output in the steam divided by the energy input in the fuel.
- If we improve the efficiency of the boiler and hold the steam use constant, as shown in the SSAT model, we can save fuel and reduce our operating expense.
- If we improve the efficiency of the boiler and hold the fuel input rate constant we can generate more steam. In our example, we could increase steam production 8,000 lbs/hr, improving the capacity of the system by 26 percent.

## Using SSAT

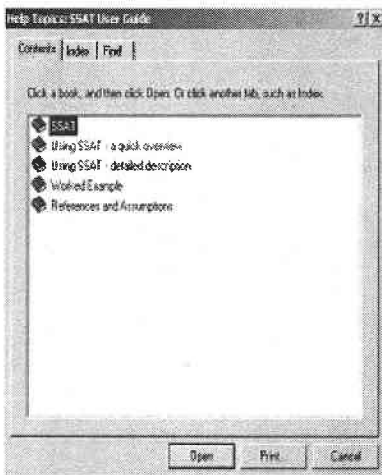
The software is free and available at the Office of Industrial Technology web site.

Originally we thought that facilities would be able to download the tool and use it to evaluate their system.

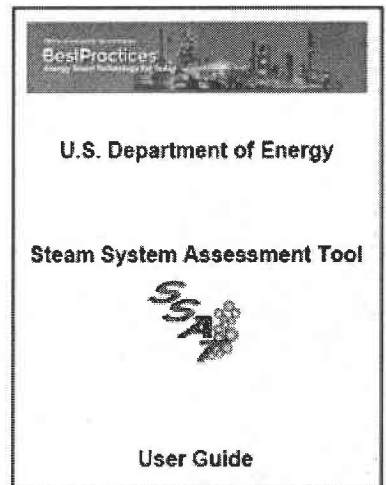
We have found that it takes a good steam system background to be able to use the tool effectively and the Department of Energy provides one day end user courses and they provide a list of Certified Steam System Specialists. These are people that have attended intensive training on the use of the software tools and have then been tested on their knowledge.

## Two Types of SSAT "Help"

On-line Version



Text Version



## For Further Information

Tony Wright, Oak Ridge National Laboratory: phone: 865-574-6878  
fax: 865-576-6642 – email: [wrightat@ornl.gov](mailto:wrightat@ornl.gov)

Best Practices Web Site Address: [www.oit.doe.gov/bestpractices](http://www.oit.doe.gov/bestpractices)

"Steaming Ahead" Web Site Address: [www.steamingahead.org](http://www.steamingahead.org)

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