THE INVESTIGATIONS OF A PECULIARITIES OF PYROCARBON GAS PHASE DENSIFICATION OF POWDERS OF THE CATALYTIC CARBON FORMATIONS (CCFs), OBTAINED ON NICKEL

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Investigations on gas-phase densification of the catalytic carbon formations (CCFs), obtained on nickel, using the method of radially driven pyrolysis zone were carried out. Straight dependence of the brittle strength of the CCFs, bonded with pyrocarbon (CCFBPyC), from the CCFs morphology, was shown. It was determined, that the result of decreasing of an amount of fibrous, fine-grained CCFs component is the increasing of strength of the pyrocarbon matrix . For the first time, carbon/carbon composite materials (CCCM) without cracks, which contain refined or not-refined from nickel, carbon nanomaterials (CNM), were obtained.

INTRODUCTION

Discovering of fullerenes in 1985 [1] and developing the technology of obtaining them in macroscopic amounts had initiated a systematic research of carbon surface structures: fullerens, single-walled (SWNT) and multi-walled (MWNT) carbon nanotubes, carbon nanofibers (CNF) and carbon nanomaterials (CNM), which include these structures, amorphous carbon or graphite. Many methods of producing SWNTs can be combined into 2 groups: sublimation - desublimation of graphite and catalytic pyrolysis of gaseous (the so-called CVD process), liquid and solid hydrocarbons and aqueous solutions [2-4]. In the National Science Center Kharkov Institute of Physics and Technology (NSC KIPT) the first experiments on the synthesis of SWNTs by the CVD method were carried out in 1982-1987 [5], at a gas-phase installation "AGAT-1.6". Later on, the numerous studies of the methods of obtaining, properties and areas of practical application of SWNTs and CNM, based on them, were carried out on the installations AGAT-1.6, AGAT-2.0, AGAT-3.2 [6-9]. Almost all SWNTs described in the literature are covered at both ends by catalyst and CNM particles. Cleaning the tubes from catalysts and impurities and opening their cavity is carried out by various oxidizing methods. CNM, obtained in NSC KIPT by the catalytic pyrolysis of methane or propane-butane on the transition metals-Fe, Co, Ni, in the temperature range 600...800 °C, using CCFs, as a carrier, in most of the cases were not cleaned and were not opened. Therefore, they are conglomerates of entangled MWNTs and 30...40 wt.% of the soot, with catalyst particles encapsulated in them [10]. In the NSC KIPT, these conglomerates were named catalytic carbon formations - CCFs. When they are ground, a black powder with particles of irregular shape, mainly fibrous and acicular, with a large (up to 40 wt.%) fraction of less than 50 µm, is formed. An analogue of this CCFs is the material "Taunit" produced by "Nano-TechCenter Ltd", Tambov [11, 12]. It is a black powder of CNT agglomerates with the dimensions of $40...60 \mu m$, bulk density $0.42...0.45 \text{ g/cm}^3$ and pycnometric density -1.6 g/cm^3 . It is obtained by the CVD

method, in propane-butane, at T = 650 °C, in a vertical cyclic reactor on a NiO-MgO catalyst, with purification in 30% HNO₃ solution and ultra-sonic dispersion in distilled water. The CCFs and "Taunit" microstructures are shown in Fig. 1.



Fig. 1. Micrographs of materials: a - CCFs NSC KIPT, scale division $-10 \mu m$; b - "Taunit"

Earlier, including within the framework of STCU projects No 293, 1870, a number of experiments were carried out on the deposition of pyrocarbon (PyC) from methane or propane-butane, both on mixtures of graphite powders with Ni, Co, Fe, and on CCFs containing these metals. When obtaining a carbon-carbon composite material (CCCM), in the form of CCFs bonded with PyC (CCFBPyC), both isothermal and thermogradient densification with pyrocarbon, by the method of radially driven pyrolysis zone, was used.

Heating of the CCFs in the experiments, conducted by this method, was carried out either by the heaters or by the direct passing of an alternate current through the CCFs. In the experiments, various technological methods were used to prevent cracking of the CCFBPC. In the most of the cases, a material without cracks, chips and ruptures was not obtained, due to its brittle fracture– Fig. 2.

No single mechanism of destruction of the CCFBPC had been identified. It was assumed that the main reason is the swelling of the material, not hardened by PyC, due to the formation of CCFs in it, at temperatures above 600 °C. The reasons for the destruction could also be:

 fibrous structure of CCF powders, which promotes their agglomeration (including forming of an anisotropic structures), during blanks moulding;

- the difference of the coefficients of linear thermal expansion (CLTE) of the CCFs, CCFBPyC and materials involved in the process of densification of the CCFs with PyC: graphite, PyC, graphite bonded with pyrocarbon (GBPyC), asbestos cloth, densificated with PyC, Mo or CCCM heater (Fig. 2), etc.;

- decrease of the quantitative yield of PyC in the pyrolysis zone (up to the formation of the soot) from a mixture of methane and hydrogen, formed during catalysis [13] and, as a consequence, a decrease in the strength of the CCFBPyC;

- adsorption of hydrogen on the catalyst and CCFs [14], with the possible formation of closed gas inclusions, which, as in the case of hydrogen embrittlement of metals, can be detonators of destruction, when internal and external mechanical and thermal stresses appear.



Fig. 2. The nature of cracking in CCFBPyC: a – *with Mo heater; b* – *with CCCM heater*

The aim of this study was to obtain CCCM CCFBPyC without cracks, by direct passage of alternate current through the CCFs, for further research and practical application.

EXPERIMENTAL PROCEDURE

The CCFs powders were obtained by their production on Ni powder, with a specific surface of 0.8 m²/g, at T = 800 °C, in a methane medium. The production of CCFs was carried out in an AGAT-3.2 unit, in a "shaft furnace" **ShF** [9]. As a catalyst carrier, the CCFs were used themselves. Powders were ground manually to a fraction of less than 315 µm.

In the experiments were used CCFs powders from the processes ShF-10, ShF-13, ShF-16, with the receipt time: 59, 64 and 61 h, pycnometric density ρ_{PCN} : 2.14, 2.09, and 2.04 g/cm³, concentration of Ni (C_{Ni}) –3.00; 2.47; 1.64 wt.%, respectively, and Ni-free powder from the process ShF-16 – ShF-16R, with $\rho_{PCN} = 1.97$ g/cm³, C_{Ni} = 0.03 wt.% (exp. 3), $\rho_{PCN} = 1.96$ g/cm³, C_{Ni} = 0.0122 wt.%. (exp. 4) – Table 1. Removal of Ni from ShP-16 was carried out by thermal refining in a vacuum of 10^{-3} atm, in CCCM tooling [15], at T = 2650 °C, during the 0.5 h.

 C_{Ni} in CCFs was determined by its ash content, proceeding from the Ni content in NiO = 78.58 wt.%. The ash content was determined after the oxidation of CCFs in air, at T = 900 °C, during the 54...56 h.

The main characteristics of "filler - binder" systems are the particle size distribution and their surface area. The size distribution of the CCFs particles was measured by sieve analysis, on a vibrating sieve "029", according to a standard technique. During the analyzes, it was found that the fractions of CCFs less than 200 µm are agglomerated. The maximum size at which selfdestruction of the CCFs agglomerates did not occur was ~ 100 μ m (see Table 1), which is consistent with the results of [16]. Therefore, to prevent agglomeration, fractions of CCFs less than 200 µm were sieved by hand, with loading 10 duralumin nuts M10, into each sieve with CCFs (see index n, Table 1). The size distribution of the agglomerated CCFs, in the powder prepared for densification with PyC, could be determined only by the BET method. Due to the lack of equipment for its production, this characteristic of the powder was not determined. For the same reason and also because of the lack of information about the effect of the specific surface area on the mechanical properties of the CCFBPyC, its measurement was not planned before the experiments. Instead, for a comparative assessment of the CCFs powders, the density of their "free" packing - ρ_{FREE} , the density after compaction – ρ_{COMP} and pycnometric density – ρ_{PCN} (determined according to the standard method in kerosene) were measured by the well-known standard methods (see Table 1).

To load the powders, containers were made in the form of single-layer shells of AT-3 asbestos cloth (exps. 1-3) and carbon fabric URAL-T-22 (exps. 4-5), impregnated with 50% water solution of PVA, with a bottom fixed in them. The top of the container was closed with a lid on a loose fit. The bottom and the cover were made of graphite EG-0 (exps. 1-4) and GBPyC-EG-0 (exp. 5), with conical current concentrators in CCFs, Ø 20x10 mm. Current concentrators were used to facilitate the formation of a central electrically conductive cord in the blank, in the initial period of its PyC densification. In the middle of the shell, a paper cup for the TCA quartz cover was fixed (Fig. 3). The blanks were molded by vibration densification of dry CCF powder, got filled into a container without a lid, on an IV-107 vibration stand, during the 5 min, in a place with a maximum vibration amplitude - in exps. 1-3 and strictly in the center - in exps. 4-5. The lid was installed in the container before the end of its compaction on the vibration stand. Densification of CCFs with pyrocarbon was carried out in a gas-phase unit AGAT-1.6, in a methane medium with an overpressure of 300 mm w.c., by the method of radially driven pyrolysis zone, with direct passage of alternate current through the CCFs and the following parameters: the speed of the pyrolysis zone: $v_{PZ} = 2 \text{ mm/h}$ (exp. 1) and 0.5 mm/h (exps. 2–5), the temperature in the pyrolysis zone: $T_{PZ} = 900$ °C. At the beginning, middle and end of the process, the temperature distribution along the container radius was measured, with the calculation of the temperature gradient ΔT . In the middle of the process, to increase the densification time and the final density of the CCFBPyC, a thermocouple (TCA) was pushed into the pyrolysis zone with $T_{PZ} = 950$ °C (exps. 3–5).

Cooling of the container in the exps. 1, 2 -unregulated, with speeds – 7000 and 1020 °C/h, in exps. 3-5 - adjustable, with speed 150 °C/h. Mechanical processing of the CCFBPyC was carried out on a 1K62 lathe.

Table 1

Experiment No														
			1		2	3		4						
Brand of powder		ShP-10		ShP-13		ShP-16R		ShP-16R		ShP-16		EG-0, exps. 4 , 5		
Fraction, µm		0-315 μm		0-315 μm		0-315 μm		50-315 μm	0-315 μm	50-315 μm	0-31	5 µm	50-200 μm	
n of	> 630 400–630	0.0		0.0		0.0		0.0		0.0	0.0		0.0	
itio	315-400	0.0	0.1	0.2	0.1	0.1	0.1	1.1	0.1	0.3	0.1	0.0	0.0	
ISO	200 215	21.4	21.3	21.5	22.6	21.0	20.3	29.0		31.0	20.5	19.9	3.8	
np er	200-313		n		n		n					n		
co vde	100, 200	24.7	24.4	25.2	27.1	26.5	25.5	37.1	66.4	36.7	27.9	27.2	45.4	
nal	100-200		n		n		n					n		
itio	50, 100	0 100 31.6	31.6	14.0	22.1	13.3	15.3	10.9	27.0		28.6	30.5	11.6	38.3
rac	30-100		n		n		n					n		
щ	< 50	22.3	40.2	31.0	36.9	37.1	43.2	5.8	33.5	3.4	20.9	41.3	12.5	
C _{Ni} , weigt %		3.	00	2.47		0.03		0.0122 (0.021<50 μm)		1.64	.64 $\frac{1.79}{(1.9<50 \ \mu m)}$			
receiving t, h		5	i9	6	54	61 and	1 0.5 h, at	T = 2650) °C					
oxidation t, h		5	54	5	54	54		56	_	56	5	54	—	
$a = a/am^3$		2.14 2.14		2.09		1.97	EG-0,	1.96 (1.98<50 μm)		2.04				
ρ_{PCN} , g/cm										(2.06<50 µm)		m)		
$\rho_{\text{FREE}}, \text{g/cm}^3$		0.	37	0.46		0.53	0-30µm	0.55		0.52				
$\rho_{\rm COMP}$, g/cm ³		0.	47	0.60		0.68	0.64	0.63		0.59			0.78	
U	$\rho_{GBP,}$ g/cm ³	1.38		1.63		1.70	1.74	1.66		1.66				
3Py	ρ_{PCN} , g/cm ³	1.	63	1.77		1.76	1.94	1.81	-	1.82] –			
EE	Porosity, %	14	4.6	8	.0	3.5	10.4	8.1		8.8			_	
ŭ	δ, PyC, μm	0.5	-1.0	3	-5	0.5-1.0	_	7–30		7–30				

CCFs, CCFBPyC parameters in experiments 1-5



1, **7** – Supports, EG-0; **2**, **5** – Current concentrators: exps. 1-4 - EG-0; exp. 5 – GBPyc- EG-0; 3 -Shell: exps. 1-3 - AT-3; exps. 4-5 - URAL-T-22; 4 - CFs, Ø 70 mm, exp. 1 - ShP-10; exp. 2 - ShP-13; exps. 3, 4 – ShP-16R; exp. 5 – ShP-16; 6 – Shell retainer; 8 – Thermal insulation of the supports, AT-3; 9 – Screen AT-3, 1 layer; 10 - Buffer, Ø 70 mm, EG-0, exp. 3 – 0...50 µm; exps. 4-5 - 50...200 μm

Fig. 3. Shemes of experiments: a – 1–8 – exp. 1; 1–9 – exp. 2; 1–10 – exp. 3; b – exps. 4–5

Densities (ρ_{GBP} , ρ_{PCN}) and open porosity (P) of CCFBPyC was measured by the hydrostatic method, after boiling in water for 4 h (see Table 1). CCFBPyC polished sections were made on a grinding machine. The

microstructure of CCF and thin sections of CCFBPyC were analyzed on microscopes MBS-10 and MMR-4. The phase composition of CCF was investigated by

X-ray structural analysis (diffractometer DRON-1.5, CuKα radiation, Ni filter) [2].

RESULTS AND DISCUSSION OF EXPERIMENTS

Due to the limited amount of starting material and the unidentified mechanism of destruction of the CCFBPyC, 5 consecutive experiments were carried out with the analysis of the results and the adjustment of the conditions for their conduct after each experiment.

EXPERIMENT 1

In experiment 1 (see Fig. 3,a), powder from the **ShP-10** process was used. The parameters of the CCFs and CCFBPyC are given in Table 1.



Fig. 4. Cracks at the ends of the container



Fig. 5. Density distribution along the container radius: 1 - CCFs ShP-10, $v_{pz} = 2$ mm/h; $2 - EG-0, 0...200 \ \mu m, v_{pz} = 0.5$ mm/h

PyC densification was carried out according to the mode: $T_{PZ} = 900$ °C, $v_{PZ} = 2$ mm/h. A high v_{PZ} was set to prevent the breakage of the blank by the formed CCFs. When measuring the temperature distribution along the radius (**R**) of the container, with the radius of the pyrolysis zone (**R**_{PZ}) equal to 35 mm, the blank, within 10 minutes, underwent a thermal shock: 900...700...900 °C, in a compressed state, with rates of decrease/growth T - 2400 °C/h on the surface and 6000 °C/h – in the center. The blank was cooled at a rate of ~ 7000 °C/h.

After turning the container, symmetrical cracks were found at its ends adjacent to the current concentrators of the bottom and lid (Fig. 4). The cracks are obviously the result of thermal shock and abrupt cooling of the blank.

The distribution of density along the radius of the CCFBPyC in the section at the middle of the container height is given in Fig. 5. The low density in the range of radii 10...20 mm is due to the premature blocking of the

transport porosity of the CCFs both the PyC, at high v_{pz} and T > 860 °C and the CCFs, at T < 860 °C. High temperature gradients ΔT at the beginning of densification (curve **3**, Fig. 6, Table 2) are determined by the presence of up to 40 wt.% of low-heat conductive soot [10] and their low packing density - 0.47 g/cm³. This density is due to the high content of a finely dispersed fibrous fraction (40 wt.% < 50 µm, see Table 1) and anisotropic stacking of CCF agglomerates, when forming the blank on the vibrating stand (exp. 3, Fig. 8,f). Comparison of the temperature distribution in the CCFs and in analogues of its structural components – soot and finely dispersed hammer pyrocarbon, which forms an anisotropic packing during molding (curves **2** and **1**, Fig. 6), allows us to consider this assumption quite justified.

EXPERIMENT 2

High temperature gradients in exp. 1, due to the both high v_{PZ} and low thermal conductivity of the CCFs, led to an uneven distribution of the density of the CCFBPyC along the radius of the container.



Fig. 6. Temperature distribution (T)along the container radius (R) in exp.1

Table 2

Temperature gradients in experiment 1										
Curve	R _{P7} .		R , mm							
No	mm		10	15	20	25	30	35		
1	5	ΔT ,	12	16	18	22	26	16		
2	5	°C/	6	8	14	18	20	24		
3	5	mm	9	1	4	19.5		22		
4	17		11	13	20	21	27	27		
5	35		_			19	22	30		

Therefore, in exp. 2, in order to prevent premature blocking of the transport porosity, it was decided to reduce the values of technological parameters responsible for the high rate of temperature rise in the zone of carbon formation $-\Delta T$ and v_{PZ} . A decrease in ΔT expands the zone of carbon deposition, but earlier starts the process of self-deactivation of the catalyst and reduces the yield of CCFs in the volume of the blank. The blocking of transport porosity occurs, therefore, later. This contributes to an increase in the thickness of the PyC layer and an increase in the strength of CCCM. To reduce ΔT , a screen 9 of 1 layer of asbestos cloth AT-3 was installed in 25...30 mm from the surface of the container (see Fig. 3,a). v_{PZ} was reduced to 0.5 mm/h, taking into account the uniform distribution of density along the radius of the container, after densification of EG-0 graphite powder, fraction 0...200 µm, at this rate – dashed curve 2, Fig. 5.

CCFs **ShP-10** were replaced by CCFs **ShP-13**, because their mass was enough to carry out at least 2 experiments. The parameters of the CCFs and CCFBPyC are given in Table 1.

The PyC densification was carried out according to the mode: $T_{PZ} = 900$ °C, $v_{PZ} = 0.5$ mm/h. The pyrolysis zone was "pulled" by 3 mm beyond the outer surface of the CCFs (R = 38 mm). At this point, the heating of the blank was inadvertently turned off and then turned on. The billet was cooled from 900 to 300 °C at a rate of 1200 °C/h and heated, in a compressed state, to 900 °C at a rate of 3000 °C/h, with the following rising of the T, at this point, from 900 to 1050 °C, for 10 h. This resulted in a significant PyC densification of the asbestos shell of the container. The billet was cooled from 1050 to 150 °C at a speed of 1020...450 °C/h.

After being removed from the pyrolysis chamber, the container was intact. A day later, a vertical crack appeared along the entire height. After turning to Ø 67 mm, at the ends adjacent to the current concentrators, the same cracks were found as in the experiment 1 (see Fig. 4), on the outer surface – a network of longitudinal and transverse cracks (Fig. 7). Longitudinal cracks

and cracks on current concentrators are the result of thermal shock. Transverse cracks were formed due to the difference between the CLTEs of the CCFBPyC and the shell of the container, significantly densified with PyC.



Fig. 7 Cracks in the CCFBPyC, ShP-13

There was no decrease in ΔT when installing the screen and increasing ρ_{COMP} of CCFs from 0.47 to 0.60 g/cm³ (Fig. 10, exp. 4, curves 1 and 2). This is most likely due to the lower heat conductivity of the CCFs **ShP-13**, compared to the CCFs **ShP-10**, because of the longer time of its production (**64** and **59** h) and the higher soot content.



Fig. 8. The nature of the destruction of CCFBPyC based on thermally refined CCFs **ShP-16R** (exp. 3): a – the diameter of the compacted PyC billet is 75 mm; b - f – the diameters of the component parts of the billet, after turning are equal to 67 mm



Fig. 9. The general view of graphite powder (a) and CCFs (b, c)

EXPERIMENT 3

According to literature data [2], annealing of CNTs in vacuum already at 1500...1800 °C cleans them of the catalyst and impurities and improves the structure. In this connection, in experiment 3, the CCFs from the process **ShP-16**, purified from **Ni** by thermal refining in a vacuum of 10^{-3} atm, at 2650 °C, for 0.5 h [15] – **ShP-16R**, were used. The parameters of the CCFs and CCFBPyC are given in Table 1.

When preparing the exp. 3 surface cracking in the blank of the exp. 2 had not yet been identified. Therefore, to obtain the results comparable with exp. 2, the blank was molded in an asbestos shell **3** and screen **9** was installed (see Fig. 3,a). The CCFs was not enough to fill the whole container, therefore, buffer **10** of EG-0 powder, with fraction $0...50 \mu m$ was filled and shaken under the lid (see Fig. 3,a).

PyC densification was carried out according to the mode: $T_{PZ} = 900$ °C, $\upsilon_{PZ} = 0.5$ mm/h. At $R_{PZ} = 22.5$ mm, a thermocouple (TCA) was introduced into $R_{PZ} = 15.5$ mm, with $T_{PZ} = 950$ °C. Further, at $R_{PZ} = 18$ mm, in the case of emergency shutdown of the installation, the container was cooled from 950 to 300 °C with the velocity = 1300 °C/h, with its subsequent heating to 950 °C, with the velocity = 3900 °C/h. Cooling was adjustable, with the velocity = 150 °C/h. The blank, removed from the pyrolysis chamber, divided into 2 parts (CM. Fig. 8,a), due to the thermal shock, in a compressed state, at $R_{PZ} = 18$ mm.

The experiments were stopped to analyze the causes of the destruction. The following studies were carried out:

1. A workpiece with Ø 75 mm was turned on a lathe to Ø 67 mm, cut into component parts and photographed (see Fig. 8).

Above the bottom current concentrator, the same cracks were found as in the experiment 2 (see Fig. 8,b), with their transition into the workpiece (see Fig. 8,c). Delamination and cracks were found in the CCFBPyC, at the junction with the GBPyC-EG-0, with their transition to the GBPyC (see Fig. 8,d). There were no cracks in the GBPyC-EG-0 buffer, under the current concentrator (see Fig. 8,e). The fracture surface of the CCFBPyC obviously repeats the structure of the CCFs stacking, which was formed on a vibration stand, with the orientation of the particles perpendicular to the workpiece axis (see Fig. 8,f). The opalescent fracture surface indicates about the separation of the CCFBPyC along the grain boundaries, that, most likely, can occur with a small thickness of the PyC layer at these boundaries. Destruction of the workpiece in the exp. 3 (and the workpiece shown in Fig. 2,b) happened in the middle of the process, and not at the end, as in exps. 1, 2. The cracks in it should have been filled with either the soot, densified with PyC, or PyC. This, however, did not happened and, quite possible, due to the composition of the gas medium (excess of hydrogen) both in the volume of cracks and in the transport porosity of the CCFs, namely:

 – excess hydrogen in cracks can be formed due to its flow from the pyrolysis zone into the volume of cracks; - the entangled, finely dispersed structure of the CCFs can hinder the diffusion of methane into the pyrolysis zone both during the formation of the CCFs and its gas-phase densification with PyC, forming a gaseous medium with an excess of hydrogen, the inhibitory effect of which on the formation of PyC is given by P.A. Tesner in the monograph [13]. Indirect confirmation of difficult diffusion of methane can be:

 during the formation of CCF – 30...40 wt.% soot in the composition of CCFs [10];

– during gas-phase densification PyC – data of the RF patent No. RU 2568733 [17], according to which in a frame with a density of 0.6...0.65 g/cm³, based on low-modulus carbon fibers, it is impossible to ensure a content of catalytically deposited carbon of more than 4.2 wt.%, since with an increase of its content, the diffusion rate of carbon-containing gas into the pores of the framework sharply decreases.

2. It was found that CCFs, with fractional composition of 0...50, $0...315 \mu$ m, adhere to each other, forming stable slip planes (Fig. 9,b,c), which promote agglomeration of CCFs into anisotropic structures, during formation of the blanks. In graphite EG-0, such stable planes are absent (see Fig. 9,a).

3. Microsections of the samples from the middle of the blanks from the exps. 1–3 were made. On the sections from the exps. 2, 3, a close-packed structure of large grains (with an average size of 200x200 μ m) is observed in a monolith of small ones, with a PyC layer thickness at the grain boundary: **0.5**...**1.0** μ m – in exps. 1,3; **3...5** μ m – in exp. 2. Closed porosity of the workpiece from the exp. 3 is elongated along the radius (laying the CCFs perpendicular to the axis, during molding). On the section from exp. 3, a chain of closed pores, connected by cracks passing through the monolithic material, was discovered. This may be the evidence that the gas in closed pores is capable of creating internal thermal stresses, leading to the destruction of the material.

4. From the theory of strength it is known that the work of brittle fracture depends on the micro- and crystalline structure, test conditions and decreases with an increase in the loading rate, the presence of stress concentrators. The rate of temperature rise of workpieces compressed by current concentrators, after emergency modes, in exps. 1-3, apparently proportional to the loading rate, was 2000...4000 °C/h. Current concentrators were, at the same time, stress concentrators. In the workpiece (see Fig. 2,b), densified according to the mode: $T_{PZ} = 900 \text{ °C}$, $v_{PZ} = 0.33 \text{ mm/h}$, $C_{Ni} = 2.67 \text{ wt.\%}$, the current concentrators were replaced by a heater made of a bundle of URAL-NSh threads, but this attempt to avoid its destruction was unsuccesfull. This may indicate that the CCFBPyCs are destroyed under the action of its own stresses in the structure, and stress concentrators only promote them. Therefore, to check the possibility of destruction of the anisotropic structures of the CCFBPyCs by internal thermal stresses, samples from exp. 1 and 3 were subjected to thermal shocks in methane, with different heating and cooling rates and holding, at T_{EXP} , for 0.5 h (Table 3).

Exp. No	Temperature range	Heating rate, °C/h	Cooling rate, °C/h
1	100400	150	1500
2	30600	1700	500
3	30800	2900	60001500
4	301000	2530	7000

Modes of heat treatment of CCFBPyCs samples

Table 3

The samples did not undergo any changes, which indicated that the destruction of the CCFBPyCs occurs along the boundaries of the structural inhomogeneities of the workpiece, under the influence of external stresses.

The following conclusions were made from the analysis:

1) brittle fracture of CCFBPyCs is determined by the morphology of CCFs, namely: agglomerates of CCFs, linked by a fine fibrous fraction, create a specific finepored structure in the workpiece, which impedes the diffusion of methane into the pyrolysis zone. This structure forms a PyC matrix with a small PyC layer thickness. The strength of the matrix is insufficient to resist internal and external stresses. Therefore, the workpiece is destroyed along the boundaries of structural inhomogeneities embedded in it during molding (see Fig. 2,b; 8,f). In this regard, the isotropy of the CCFs moldings is fundamentally important. It can be provided, in particular, by manual ramming with or without shaking the container;

2) to increase the strength of the PyC matrix, it is necessary to increase the thickness of the PyC layer by increasing the transport porosity of the material. This improves the supply of methane and the removal of products of its decomposition from the pyrolysis zone. This can be achieved by: reducing the bulk density of the CCFs (manual filling without a shaker), its preliminary agglomeration with any (including PyC) binders, the introduction of pore-forming additives (salt, sugar, glycerin, PVA, phenol-formaldehyde resin, etc.), the selection of the fractional composition, in particular, the removal of finely dispersed CCFs nanostructures;

3) when using other methods of the densification of CCFs with PyC: densification without a screen, decrease in v_{PZ} (the workpiece shown in Fig. 2,b collapsed at $v_{PZ} = 0.25$ mm/h), an increase in T_{PZ} , remains and again forms on the catalyst, fine nanostructure of CCFs and low-strength PyC matrix, repeating it.

It has been hypothesized that this has been the main reason for the failure to obtain CCFBPyCs without cracking for the present time. To test this assumption, in exps. 4, 5, a fraction of $0...50 \mu m$, which consist mainly of such nanostructures, was removed from the CCFs.

EXPERIMENT 4

When preparing exp. 4, the technological factors, contributing to the brittle destruction of CCFBPyC (see Fig. 3,b), were excluded:

- the shell container **3**, \emptyset 70 mm, formed from a single-layer AT-3 asbestos cloth and used in exps. 1–3 was replaced with the shell container, made from a 1 layer of URAL-T-22 carbon fabric;

– a fraction of $50...315 \mu m$ of powder **ShP-16R**, obtained after deleting $0...50 \mu m$ fraction of this powder was used in the experiment. The parameters of CCFs and CCFBPyC are given in Table 1;

- for isolation of current concentrators from CCFs, the buffers **10** of graphite powder EG-0, fraction $50...200 \,\mu\text{m}$ were filled in and shaken on them;

- for comparability with the results of previous experiments and for alignment of the radial and vertical gradients T, screen 9 and supports 1, 7, Ø 60x100 mm, with increased electrical resistance, were installed, respectively.

The densification of the CCFs was carried out according to the mode: $T_{PZ} = 900$ °C, $v_{PZ} = 0.5$ mm/h. At $R_{PZ} = 12.5$ mm, TCA was entered into $R_{PZ} = 6.5$ mm, with $T_{PZ} = 950$ °C.



Fig. 10. Temperature distribution (T) along the container radius (R) in exps.1, 2, 4, 5 Table 4

Temperature gradients in experimet 4

Curve	$R_{\rm PZ}$,		R, mm							
INO	mm		10 15 20	20	25	30	35			
1	5	Δ <i>T</i> , °C/ mm	9	14		19.5		22		
2	5		13	15		15		16		
3	5		7	.5 9) 1		3		
4	35		2	2 4		1	1	0		
5	35		3	3.4	6	5 11		.4		
6	35		1.4	2.4	3.2	6	8	12		

Comparison of temperature distribution and ΔT (Fig. 10, Table 4) in thermo-refined and non-thermorefined CCFs, both at the beginning (curves 3 and 1, 2) and at the end of the process (curves 4 and 5, 6) indicates an increase in its heat conductivity, due to the removal of the low-heat-conductivity fraction 0...50 µm and partial graphitization, after annealing at T = 2650 °C.

After the completion of densification and turning to \emptyset 67 mm, no damage was found in the workpiece (Fig. 11). The thickness of the PyC layer in the CCFBPyC was 7...30 µm.



Fig. 11. CCFBPyC machined blanks from the exps. 4, 5

EXPERIMENT 5

Exp. 5 was carried out according to the scheme of exp. 4 (see Fig. 3,b). In the experiment, a fraction of 50...315 µm of powder ShP-16 was used, with $C_{\text{Ni}} =$ 1.64 wt.%. The parameters of CCFs and CCFBPyC are given in Table 1. Additionally, to reduce the vertical gradient *T*, the Ø of the supports 1.7 was reduced to 50 mm, and the current concentrators 2, 5 were made of GBPyC-EG-0, with a specific electrical resistance 2 times higher than that of the EG-0. The densification of the CCF was carried out according to the mode: $T_{\text{PZ}} = 900 \,^{\circ}\text{C}$, $v_{\text{PZ}} = 0.5 \,\text{mm/h}$. At $R_{\text{PZ}} = 26.5 \,\text{mm}$, TCA was entered into $R_{\text{PZ}} = 20.5 \,\text{mm}$, with $T_{\text{PZ}} = 950 \,^{\circ}\text{C}$. After densification, no damage was found in the workpiece (see Fig. 11). The thickness of the PyC layer in the CCFBPyC was 7...30 µm.

Thus, in exp. 5, it was confirmed that it is possible to obtain a CCFBPyC without cracks on non-cleaned CCFs. The insignificant content of **Ni** (1.64 wt.%) does not allow to make an unambiguous conclusion about the influence of the catalyst concentration in the CCFs on the destruction of the CCFBPyC. But, most likely, there will be no need to determine this influence, since purified CNTs and CNMs are used (and are being investigated) all over the world.

Carrying out physical-mechanical and thermophysical studies of the obtained materials will make it possible to clarify the stated assumptions.

Improvement of technologies for production and thermal refining of CNM will allow to receive at NSC KIPT up to 300 kg of CNM and up to 50 kg of purified CNM per month.

CONCLUSION

The conducted studies of pyrocarbon densification of powders of catalytic carbon formations (CCFs) on Ni showed a direct dependence of their brittle strength from the morphology of CCFs. A decrease in the amount of the finely dispersed fibrous component of the CCFs for the first time allowed to obtain CCCM blanks without cracks, based on purified and not purified from Ni carbon nanomaterials (CNM). It is necessary to take into account the low thermal strength of CCCM based on CCFs both when forming blanks and densification with PyC, namely:

 molding of CCFs must be carried out using materials, the CLTE of which is not very different from the CLTE of PyC (carbon fabric, GBPyC);

 – current concentrators (in the case of the direct passing of an alternate current through the CCFs) should not come into contact with the CCFs; - the backfill of the CCFs should be maximally isotropic and gas-permeable;

– during densification, both thermal shocks and CCFBPyC lifting/cooling rates above 200 °C/h should be excluded. Separately, the need to reduce ΔT in CCFs requires clarification.

The efficiency of the equipment developed at the NSC KIPT for the method of vacuum-thermal refining of carbon materials has been confirmed [15]. This method is more environmentally friendly than chemical cleaning. Improvement of the equipment will make it possible to clean up to 50 kg of any CNM per month at the NSC KIPT.

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ИССЛЕДОВАНИЕ ОСОБЕННОСТЕЙ УПЛОТНЕНИЯ ПИРОУГЛЕРОДОМ ПОРОШКОВ КАТАЛИТИЧЕСКИХ ОБРАЗОВАНИЙ УГЛЕРОДА (КОУ) НА НИКЕЛЕ

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Исследовано газофазное уплотнение пироуглеродом порошков каталитических образований углерода (КОУ) на Ni методом радиально движущейся зоны пиролиза. Показана прямая зависимость хрупкой прочности уплотненных порошков от морфологии КОУ. Установлено, что уменьшение количества мелкодисперсной волокнистой составляющей КОУ увеличивает прочность пироуглеродной матрицы. Впервые получены углерод-углеродные композиционные материалы (УУКМ) без трещин на основе очищенных и не очищенных от Ni углеродных наноматериалов (УНМ).

ДОСЛІДЖЕННЯ ОСОБЛИВОСТЕЙ УЩІЛЬНЕННЯ ПІРОВУГЛЕЦЕМ ПОРОШКІВ КАТАЛІТИЧНИХ УТВОРЕННЬ ВУГЛЕЦЮ (КУВ) НА НІКЕЛІ

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Досліджене газофазне ущільнення піровуглецем порошків каталітичних утворень вуглецю (КУВ) на Ni за допомогою методу зони піролізу, що радіально рухається. Показана пряма залежність крихкої міцності ущільнених порошків від морфології КУВ. Встановлено, що зменшення кількості дрібнодисперсної волокнистої складової КУВ збільшує міцність піровуглецевої матриці. Вперше отримані вуглець-вуглецеві композиційні матеріали (ВВКМ) без тріщин на основі вуглецевих наноматеріалів (ВНМ) з видаленим та невидаленим нікелем.