

UNCERTAINTY AND SENSITIVITY ANALYSIS IN TURBULENT PIPE FLOW SIMULATION

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Abstract. In this study, we would like to evaluate and improve the performance of Wall-Modeled Large-Eddy Simulation (WMLES) on the modeling of a pipe flow for which Direct Numerical Simulation (DNS) data is available [1] and considered as a reference for further comparisons.

Models used in WMLES may raise problems of accuracy which come from the uncertain values of model parameters and model simplifications. In this study, we focus firstly on the impact of the model parameter uncertainties on the simulation results, and then on the reduction of these uncertainties via data calibration. These studies using sampling-based approaches can be unaffordable when coupled with a high-fidelity simulation that requires several CPU hours for a single execution. To reduce the computational cost while maintaining a target accuracy, we propose to build surrogate models based on Gaussian Processes for simulations outputs, and replace the simulator for evaluating the large size sampled sets.

For this study, a CFD-UQ methodology is developed which couples our internal UQ tool and a CFD solver. It has been applied on a turbulent pipe flow case that allows us to validate its implementation.

1 INTRODUCTION

In the last decades, supported by the rapid development of computational capacity and the improvement of mathematical modeling, a significant increased usage of numerical simulation tools like Computational Fluid Dynamics (CFD) for the analysis and design of numerous engineering applications can be observed. The use of CFD in automobile engineering becomes more common, especially the Large-Eddy Simulation (LES), for its ability to reproduce the numerous coupled phenomena in internal combustion engines. However, in such simulations, uncertainties can arise from different inputs of the simulation, including material properties, initial and boundary conditions, physical models and numerical resolution, which question the quality of the results obtained and disturb the associated analysis.

To obtain reliable results, it is necessary to study the impact of all these uncertainties onto the final solution. A possible approach is the application of Uncertainty Quantification (UQ) tools, which allows to propagate uncertainties related to different factors (inputs and parameters, ...) of a simulator (i.e. the computational code) to its outputs. The use of UQ in CFD application has attracted attention from various domains, typically in nuclear engineering where CFD is more and more used as a tool for design and safety issues and related uncertainties need to be well controlled [2], and also in aerospace applications [3] and aircraft design [4]. UQ has been introduced in experimental research [5] in automobile engineering, while numerical work with UQ is still challenging on real systems like internal combustion

engines. Therefore our motivation is to develop a feasible UQ methodology for engine CFD applications.

UQ methods can be generally divided into 2 categories : intrusive and non-intrusive UQ methods. In intrusive approaches, the stochastic description of the parameter is integrated within the numerical formulation which may exhibits algorithmic difficulties. In contrast, non-intrusive approaches are sampling based, and the simulator is used as a black box. Therefore they are usually used in CFD applications.

The most known non-intrusive UQ method is the Monte Carlo sampling which is very straightforward and easy to implement. However, it requires a large number of simulator runs to achieve accurate statistical results due to its low convergence rate, and becomes intractable for CFD applications. One technique is to replace the CFD code by surrogate models characterized by fast response time. Only a limited number of simulations is necessary to construct surrogate models which provide an approximation of the relationship between simulation input and output vectors. Further UQ analysis can fully rely on predictions provided by these surrogate models. A popular surrogate model in UQ is based on Gaussian Processes (GP) which allow flexible approximations with an intrinsic control of estimation errors [6].

The present study aims to develop a non-intrusive CFD-UQ methodology based on existing UQ techniques to quantify accuracy, robustness and sensitivity of CFD simulations. Analysis is based on surrogate models of Quantities of Interest (QoIs) extracted from simulations and chosen for UQ study. Its application to engine simulations remains difficult as the engine flow is strongly non-stationary and complex, and uncertainties can come from not only physical models used in simulation for which parameters are not always known and can be case-dependent, but also from boundary conditions obtained from experimental measurements for which uncertainties are not well estimated. For validation purposes, this methodology is applied on a relatively simple case : a turbulent pipe flow, which features typical conditions of engine flows in intake and exhaust ports.

The structure of this paper is as follows: in Section 2, basic concepts of LES modeling are described, and in Section 3 detailed description of the test case used for the evaluation of the CFD-UQ methodology is provided. Section 4 presents results of the UQ analysis.

2 LES modeling

In LES, filtered Navier-Stokes equations are solved. The Favre-filtered momentum equation for compressible flows can be written as follows [7] :

$$\frac{\partial \bar{\rho} \tilde{u}_i}{\partial t} + \frac{\partial \bar{\rho} \tilde{u}_i \tilde{u}_j}{\partial x_j} = - \frac{\partial \bar{p}}{\partial x_i} + \frac{\partial \bar{\tau}_{ij}}{\partial x_j} - \frac{\partial}{\partial x_j} (\bar{\rho} (\widetilde{u_i u_j} - \tilde{u}_i \tilde{u}_j)) \quad (1)$$

where $\bar{\rho}$ is the density, \bar{p} is the pressure, u_i the i^{th} component of the velocity field, $\bar{\tau}_{ij}$ is the viscous shear stress tensor and $\bar{\rho} (\widetilde{u_i u_j} - \tilde{u}_i \tilde{u}_j)$ is the unresolved subgrid stress tensor τ_{ij}^{SGS} . τ_{ij}^{SGS} needs special modeling to close the equation, therefore subgrid stress model is necessary in LES.

2.1 Closure of the Favre-filtered momentum equation

The Smagorinsky SGS model is chosen for SGS modeling in this study. It is the simplest model and has been proven to perform reasonably well [8]. The basic principle of such a model is to account for the additional diffusivity inherited from the turbulent flow structures that are smaller than the filter size, by adding explicitly in the conservation equations an additional, non-physical viscosity, called turbulent or eddy viscosity ν_t . It assumes that it is possible to express the subgrid stress tensor τ_{ij}^{SGS} in a similar way

to the shear stress tensor $\bar{\tau}_{ij}$ following :

$$\bar{\tau}_{ij} = 2\bar{\rho}v_t(\tilde{S}_{ij} - \frac{1}{3}\delta_{ij}\tilde{S}_{kk}) \quad (2)$$

$$\tau_{ij}^{SGS} - \frac{1}{3}\delta_{ij}\tau_{kk}^{SGS} = 2\bar{\rho}v_t(\tilde{S}_{ij} - \frac{1}{3}\delta_{ij}\tilde{S}_{kk}) \quad (3)$$

where \tilde{S}_{ij} is the strain rate tensor computed as $\tilde{S}_{ij} = \frac{1}{2}(\frac{\partial \tilde{u}_i}{\partial x_j} + \frac{\partial \tilde{u}_j}{\partial x_i})$.

Using the Boussinesq hypothesis [8], the eddy viscosity v_t is modeled as $v_t = (C_s\Delta)^2\sqrt{2\tilde{S}_{ij}\tilde{S}_{ij}}$, where Δ is the filter size of LES and C_s the Smagorinsky constant. The value of C_s is not universal and depends on the flow's nature. A typical value of C_s is 0.18 which is determined from the homogeneous isotropic turbulence. In practice, its value may vary from 0.1 to 0.23 [9].

2.2 Wall shear stress modeling

When applying a wall-function boundary condition, the wall-normal velocity is set to zero and the wall shear stress is imposed. The friction velocity u_τ is obtained by solving iteratively the logarithmic law of the wall :

$$u^+ = \frac{1}{\kappa} \ln y^+ + B, \quad y^+ > 30 \quad (4)$$

where $u^+ = \tilde{U}/u_\tau$ and $y^+ = yu_\tau/\nu$. \tilde{U} is the tangential velocity at the center of the first near-wall cell, ν is the kinematic viscosity and u_τ is the friction velocity defined from the wall shear stress τ_w as $u_\tau^2 = \tau_w/\rho$. τ_w will then be used to estimate the local velocity gradient in the momentum equation.

The empirical constants in the logarithmic law, the so-called von Karman constant, κ , and the additive constant, B , are generally considered as universal. Nonetheless, there seems to be no consensus about what these universal values actually are. According to a review of previous work [10], the value of κ may vary between 0.3 and 0.45, and that of B may range from 4 to 6. Most values are extracted from experimental measurements in which errors can be important, however in recent DNS of pipe flows, different values of κ and B are also found for different Reynolds numbers [1, 11].

3 Turbulent pipe flow

3.1 Presentation of the test-case

The test-case chosen for the UQ study is a fully developed turbulent pipe flow at Reynolds number $Re = 44000$. Direct Numerical Simulation results on the same case obtained by Wu and Moin [1] can be used as reference data for the UQ study. This canonical case has been extensively used in the literature to study the physics of wall-bounded turbulence and also to develop and test numerical algorithms due its simple nature. Additionally, same kind of flows exist also in internal combustion engine, in both intake and exhaust ports (typical Re is in the order of 10^4 [12]). UQ study on this case helps us to prepare the UQ application on engine cases in the future.

The pipe's radius is $R = D/2 = 5 \text{ mm}$ and its length is $15R = 75 \text{ mm}$ as recommended in [1]. An air flow at 300 K and 1 atm is driven by fixed mass flux and is periodic in axial direction z , the corresponding averaged bulk velocity U_b is 69.3 m/s . The pipe wall is set to be isothermal and its temperature is fixed to 300 K . The pipe flow simulations are carried out using commercial CFD solver CONVERGE V2.4

[13]. For this high Reynolds number flow, WMLES is performed as it gives a good compromise between computational cost and accuracy. Detailed simulation set-up is described in the following sections.

3.2 Simulation set-up

The simulation is performed using a 2nd order Crank-Nicolson scheme for temporal integration and a 2nd order central scheme for spatial discretization. A CFL number based on convective velocity of 0.3 is used to limit the time step. The Cartesian mesh used is presented in Figure 1, as we can notice, cells close to the pipe wall are set 2 times larger than those in the inner region so that center of wall cells is located in the logarithmic region of the boundary layer. Finer grid size is used in outer regions where gradients of the filtered velocity need to be resolved. Turbulent fluctuations are located in the inner region and vanish in the near-wall region as it can be observed in Figure 1.

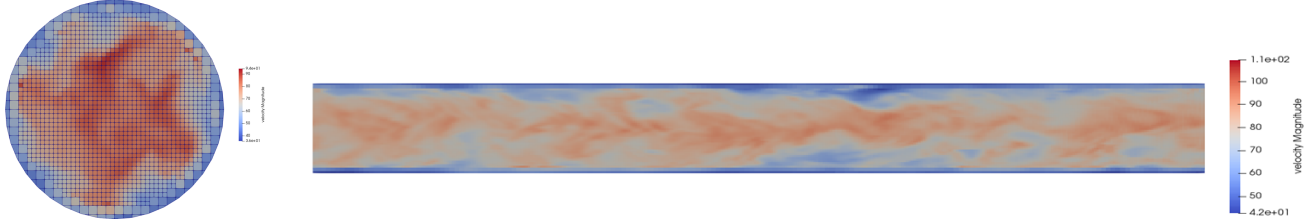


Figure 1: View of mesh on Figure 2: Snapshot of instantaneous velocity magnitude inside the pipe transversal section of the pipe

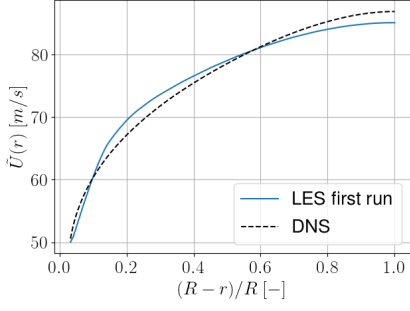
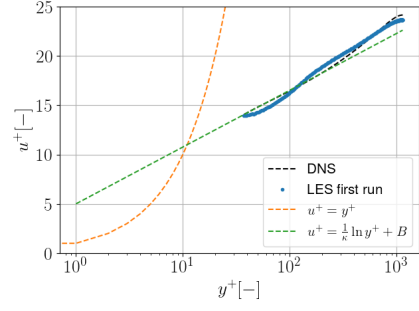
Starting from initial conditions of the constant bulk velocity U_b such that $Re = U_b D / \nu = 44000$, the flow undergoes transition and eventually becomes fully turbulent. Then, QoIs (QoIs) can be computed for further analysis.

3.3 Results of first run

Using the numerical setup described above, a first run is performed using default values in the solver $\kappa = 0.42$, $B = 5.5$ and $C_s = 0.1$. Figure 2 shows the instantaneous velocity field inside the pipe. LES well captures detailed turbulent structures of different scales.

Instantaneous velocity does not permit to characterize the flow, therefore the averaged axial velocity $\tilde{U}(r)$ in the radial direction r is computed as the averaged flow is axially symmetric. Once the flow becomes fully turbulent, the simulation continues for an additional time of $300R/U_b$, allowing a particle to travel 20 times along the pipe at the bulk velocity U_b . Statistics are collected for each time step during this period. Finally, velocity is averaged over time and axial direction of the flow for a better convergence. In the following, $\tilde{U}(r)$ states for its the time averaged value.

The averaged axial velocity \tilde{U} as a function of the normalized wall distance is presented in Figure 3, and the corresponding dimensionless profile is presented in Figure 4. The center of the first cell is located at $y^+ = 36$, well inside the log-law region. With the current configuration, the velocity profile is already comparable with that of DNS. Considering DNS data as reference, the relative error of our simulation on \tilde{U} can be quantified by a relative error $\epsilon_{\tilde{U}}$ defined as $\epsilon_{\tilde{U}} = |(\tilde{U} - \tilde{U}_{ref}) / \tilde{U}_{ref}|$. The global error on the profile we have in the first run is of 2.1%.


 Figure 3: Mean profile \tilde{U}

 Figure 4: Dimensionless mean profile \tilde{U}^+

The momentum equation of the mean flow can be written as :

$$\frac{d\bar{\tau}}{dr} = -\frac{d\bar{p}}{dz} \quad (5)$$

In the periodic fully turbulent flow, the mean pressure gradient is uniform across the flow, thus the mean shear stress is also constant. Knowing values of $\bar{\tau}$ at the pipe center $\bar{\tau}(0) = 0$ and at the wall $\bar{\tau}(R) = \tau_w$, the mean shear stress $\bar{\tau}$ is obtained as $\bar{\tau}(r) = \tau_w \cdot r/R$.

The total shear stress $\bar{\tau}_{tot}$ is the sum of 3 contributions :

$$\bar{\tau}_{tot} = \underbrace{(-\bar{\rho}v \frac{d\tilde{u}_z}{dr})}_{\bar{\tau}_{lam}} + \underbrace{(-\bar{\rho}v_t \frac{d\tilde{u}_z}{dr})}_{\bar{\tau}_{sgs}} + \underbrace{\bar{\rho}\tilde{u}_r\tilde{u}_z}_{\bar{\tau}_{res}} \quad (6)$$

where $\bar{\tau}_{lam}$ is the filtered viscous shear stress, $\bar{\tau}_{sgs}$ the subgrid shear stress and $\bar{\tau}_{res}$ the resolved shear stress.

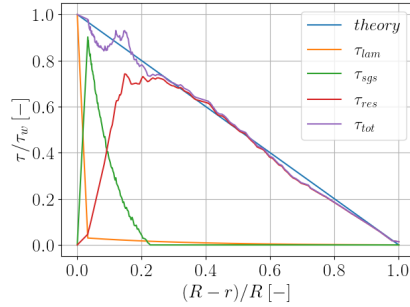


Figure 5: Shear stress distribution in wall normal direction

The time-averaged shear stress budget is presented in Figure 5, the analytical expression of the total shear stress is also plotted for comparison. Far from the wall, the total shear stress, mainly contributed by the turbulent shear stress, follows well the analytical expression. The wall shear stress is completely viscous, while in the inner region of the pipe the viscous stress is negligible. In the near wall region, the shear stress is mainly due to the subgrid stress model, which also becomes negligible far off the wall. In the vicinity of the wall, the total shear stress deviates from the analytical expression, which may be

related to the jump of cell size in this area which disturbs the estimation of the local gradient and the resolution of the momentum equation.

4 UNCERTAINTY AND SENSITIVITY ANALYSIS ON PIPE FLOW SIMULATION

In this section, the CFD-UQ methodology is evaluated on the test case described in the previous section. Only uncertainties from the 2 physical models used in LES are studied.

4.1 Methodology

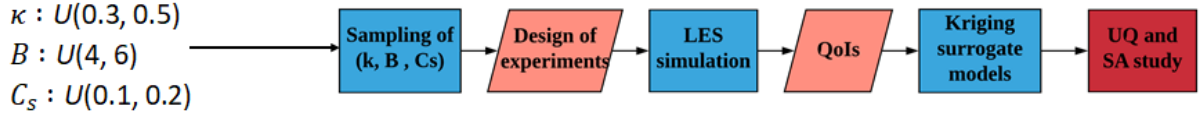


Figure 6: Workflow of CFD-UQ methodology

The Figure 6 presents the workflow of the CFD-UQ methodology used in this study. It can be divided into several parts :

- Based on prior distributions, a sampling of the parameter space is performed using Maximin Latin Hypercube method [14], leading to a Design of Experiments (DOE) of N_s samples.
- LES is then launched for each sample of DOE, providing the QoIs used in the next steps of the study.
- Surrogate models based on Gaussian Processes [6, 15] are built for QoIs. LES will not be called anymore.
- Uncertainty and sensitivity analysis are finally carried out using surrogate models built previously.

The uncertainty and sensitivity analysis allows us to investigate how uncertainties on model parameters can impact the results of simulation. Different techniques are applied :

- The sensitivity analysis is carried out to quantify the impact of the parameters on simulation results. The variance-based Sobol indices [16] are computed as measures of sensitivity by RBD-FAST method [17], chosen for its efficiency and reliability.
- Based on experimental data and prior distribution of model parameters, the data calibration aims to reduce these parameter uncertainties thanks to Bayes' theorem [18]. The resulting posterior parameter distribution (compared to the prior distribution) gives the uncertainty reduction achieved by the data integration.
- The resulting uncertainties on output parameters is simply based on the propagation of input parameters' posterior distribution obtained in the previous step, on the outputs via the surrogate models.

In the next parts, we will present the application of our methodology on the pipe flow case.

4.2 Design of experiments

We focus on the uncertainties introduced by the constant parameters of the SGS tensor and of the law-of-the-wall used in LES of pipe flow. Consistently with ranges of values found in the literature [9, 10], we define for each parameter a uniform prior distribution as follows : $\kappa \in U(0.3, 0.5)$, $B \in U(4, 6)$, $C_s \in U(0.1, 0.2)$.

Based on prior distributions, a DOE of 400 samples is generated. Similar number of samples is used for another study with also 3 parameters and associated surrogate models showed good quality [19].

4.3 Surrogate modeling

LES is then performed for all samples to compute QoIs defined in Section 3.3 : averaged velocity profile $\tilde{U}(r)$ and the averaged error $\varepsilon_{\tilde{U}}$. The results are presented in Figure 7 and Figure 8. It can be seen that $\tilde{U}(r)$ varies significantly with respect to the 3 parameters and the corresponding error as well. The reference curve of $\tilde{U}(r)$ lies well inside the variation range. The maximal $\varepsilon_{\tilde{U}}$ can reach more than 0.15 which represents an important deviation compared to the reference data.

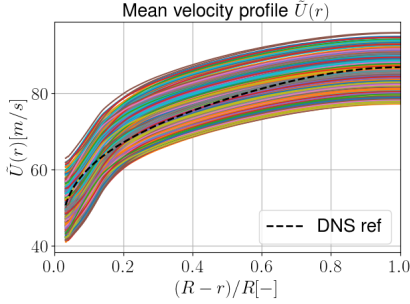


Figure 7: $\tilde{U}(r)$ extracted from LES

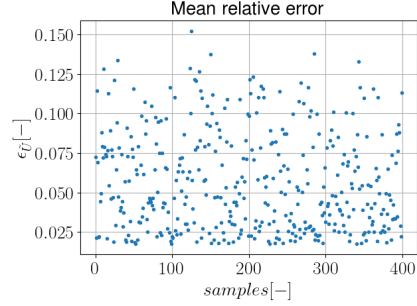


Figure 8: $\varepsilon_{\tilde{U}}$ extracted from LES

Surrogate models based on GP are then constructed for QoIs using all the samples as a training dataset : a multivariate model of $\tilde{U}(r)$ and a monivariate model for $\varepsilon_{\tilde{U}}$. Given the high cost of LES, we choose not to set a validation dataset. Instead, the leave-one-out cross-validation is done to evaluate the quality of models : the corresponding predictivity coefficient Q_2 [20] value is extremely close to 1 for all surrogate models. Obtained models are shown in Figure 9 and Figure 10, with fixed $C_s = 0.1$.

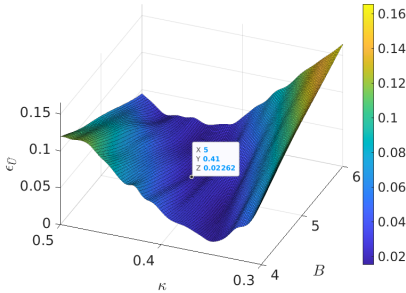


Figure 9: Response surface of $\varepsilon_{\tilde{U}}$

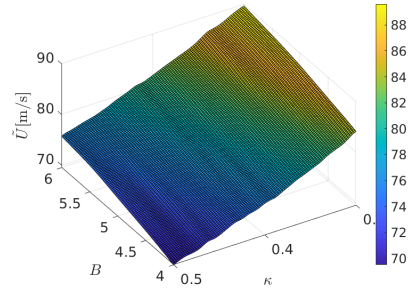


Figure 10: Response surface of $\tilde{U}(r)$ for $r = R/2$

Figure 9 shows us that the response surface of $\varepsilon_{\tilde{U}}$ is of valley shape. $\varepsilon_{\tilde{U}}$ is minimized for κ and B located at the bottom of the valley. Additionally, a couple of $\kappa = 0.41$ and $B = 5$ is found in this area and corresponds to values found from pipe flow experiments [21], which confirms our simulated results. The response surface of $\tilde{U}(r)$ at $r = R/2$ shown in Figure 10 is almost flat, and the impact of κ and B on the velocity at this point is obvious : smaller value of B and larger value of κ lead to lower velocity and

κ seems to have a relatively more important role.

4.4 Sensitivity analysis

The purpose of sensitivity analysis is to rank the input parameters according to their impact on the simulated outputs. In this part, variance-based Sobol indices are computed, which allows the quantification of the impact of the 3 parameters on the QoIs extracted from LES.



Figure 11: Sobol indices of $\epsilon_{\tilde{U}}$

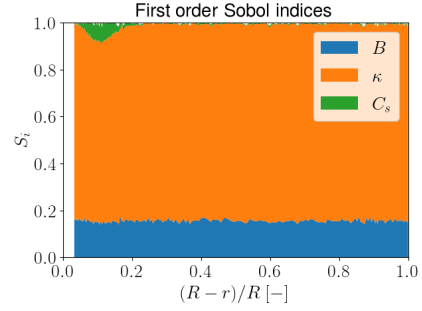


Figure 12: Sobol indices of $\tilde{U}(r)$

The sensitivity analysis is firstly done for $\epsilon_{\tilde{U}}$. Sobol indices are plotted in Figure 11. It is clear that κ is the most influential parameter for $\epsilon_{\tilde{U}}$. B alone doesn't have a significant influence but combined with κ it also takes an important part in the variations of $\epsilon_{\tilde{U}}$. Relatively the Smagorinsky constant C_s has little impact on the variations of $\epsilon_{\tilde{U}}$.

The same study is then carried out for the QoI \tilde{U} in order to study how the 3 parameters affect the velocity along the profile at different positions. Sobol indices are computed for each discretization point on the velocity profile and their values are plotted in Figure 12 as a function of the normalized wall distance. We observe that κ is still the most critical parameter as it is for $\epsilon_{\tilde{U}}$, from the near wall region to the pipe center. The influence of B is relatively less significant and is constant along the profile. C_s remains the least important parameter but interestingly it does affect \tilde{U} in the near wall region.

As a reminder, the contribution from the subgrid scale in total shear stress $\bar{\tau}_{sgs}$ is dominant in the near wall region, as we can see in Figure 5. Moreover, the region in which C_s impacts the most coincides with the one in which $\bar{\tau}_{sgs}$ is prevalent among all the contributions. This can be explained by the fact that $\bar{\tau}_{sgs}$ depends on the value of C_s as it is proportional to the eddy viscosity modeled by the SGS model. In fact, the turbulent viscosity given by the Smagorinsky model increases when approaching the wall to reach a value similar to the one obtained by the Prandtl mixing-length model [22]. Therefore, C_s can directly affect the shear stress of flow and can finally affect the velocity profile, though its impact is relatively weak compared with parameters of the law-of-the-wall model.

We can also compute the momentum thickness θ of the boundary layer using the following formula :

$$\theta = \int_0^R \frac{\tilde{U}(y)}{\tilde{U}_c} \left(1 - \frac{\tilde{U}(y)}{\tilde{U}_c} \right) dy, y = R - r \quad (7)$$

where \tilde{U}_c is the velocity at the pipe center. Using the reference \tilde{U} from DNS, the thickness θ equals to $0.089R$, i.e $\theta^+ = 106$ in dimensionless scale, which is larger than the dimensionless wall distance of the

first wall cells ($y^+ = 35$ in average). The maximal Sobol indice of C_s locates at $0.1R$ which is of the same order of magnitude as θ .

4.5 Data calibration

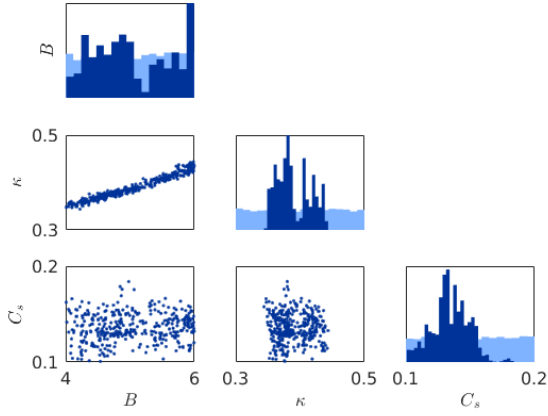


Figure 13: Prior and posterior distributions of inputs

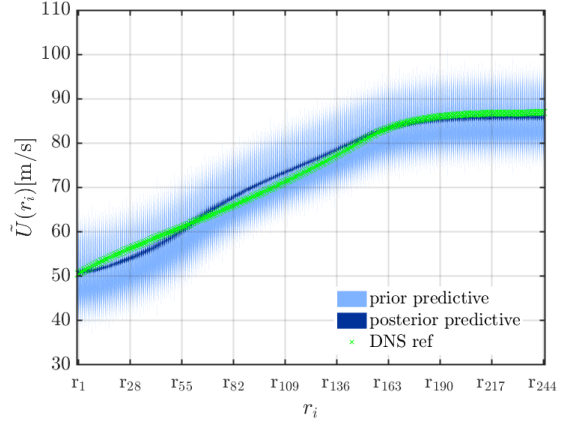


Figure 14: Uncertainty propagation on $\tilde{U}(r)$

As we can see in Figure 7, $\tilde{U}(r)$ varies a lot with respect to the 3 parameters whose uncertainties are important. To reduce these uncertainties, a data calibration is applied using the DNS velocity profile as reference data. The result is shown in Figure 13. Distributions of parameters, both prior (in light blue) and posterior after calibration (in dark blue), are presented on the diagonal. The three other graphs are joint distributions between different couples of parameters. After calibration, uncertainties are reduced for the 3 parameters as we can observe on the posterior distributions. Also, these distributions are multimodal meaning that several values of the parameters are the most likely to lead to a good data calibration: B has 2 groups of optimal values centered at 4.6 and 5.5, κ has also 2 groups of optimal values centered at 0.37 and 0.42, C_s has a very likely value at around 0.13. On the joint distribution of κ and B , a narrow zone appears and a strong correlation between κ and B can be identified.

Once prior and posterior distributions of input parameters are available, we can evaluate the corresponding distributions of the QoI $\tilde{U}(r)$ by performing uncertainty propagation. Samples are randomly generated based on prior and posterior distributions, and then propagated to the output $\tilde{U}(r)$ via surrogate model predictions. The corresponding output results are then gathered to obtain distributions of $\tilde{U}(r)$ (Figure 14).

The distribution of $\tilde{U}(r)$ obtained with prior prediction presents a significant level of uncertainty, and the one obtained with posterior prediction shows almost no uncertainty thanks to the reduction of uncertainties by data calibration. Even though uncertainties have been largely reduced on $\tilde{U}(r)$, local deviations compared to the reference data can still be observed. This indicates that the current configuration needs other improvements than data calibration to obtain better results.

We have seen that all possible combinations of κ and B allowed in posterior distributions give almost the same velocity profile, and the reason can be explained after a very simple manipulation of the law-

of-the wall. Based on the log-law we can establish a relation between κ and B :

$$B = -\frac{C_1}{\kappa} + C_2, \quad C_1 = \ln y^+, \quad C_2 = u^+ \quad (8)$$

From a LES with $\kappa = 0.41$ and $B = 5.5$ (located in the narrow zone of joint distribution in Figure 13), values of C_1 and C_2 can be determined such that $C_1 = \ln(35) = 3.55$ and $C_2 = 14.25$. In Figure 15 the curve of the equation (8) is plotted and it indeed passes through the middle of the joint distribution. Hence, a linear correlation exists between B and $1/\kappa$ which allows the error minimization on $\tilde{U}(r)$.

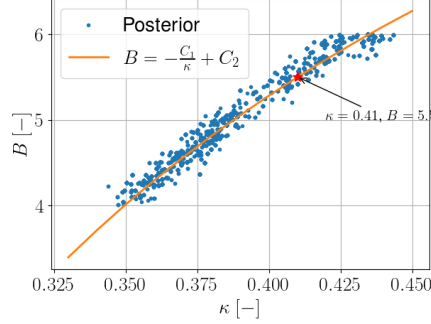


Figure 15: Joint posterior distribution of κ and B compared with equation (8)

4.6 Final tuning of model parameters

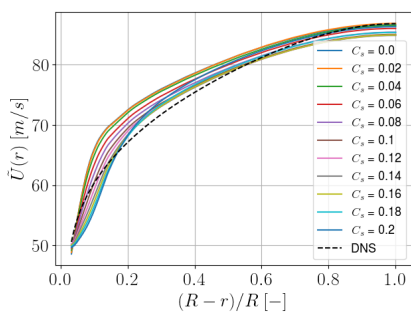
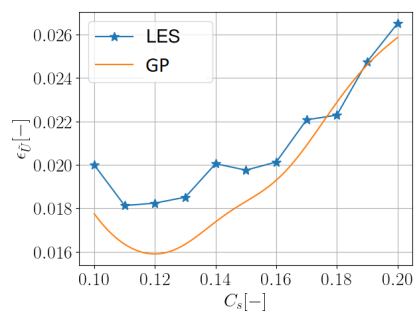
From the previous UQ analysis we have seen that the optimal choice of κ and B is not unique in this particular case. Thus, we only try to propose one possible choice for the 3 parameters that permits to obtain the optimal velocity profile in the current configuration.

The sensitivity analysis in the Section 4.4 has shown that κ and B are more critical parameters and therefore their optimal values are first determined. As no uniqueness exists in this case, we now fix the parameters $\kappa = 0.41$ and $B = 5.5$ which are likely values as shown in Figure 15. To determine the optimal value of C_s between 0.1 and 0.2, we can either rely on LES to compute the error $\epsilon_{\tilde{U}}$ for different values of C_s , or use the surrogate model of $\epsilon_{\tilde{U}}$ to predict the error for given C_s . Both approaches are adopted and the results are compared below.

Results of 11 LES are plotted in Figure 16. The variation due to the value of C_s used is relatively small, as C_s is the least influential parameter for QoIs. The corresponding error $\epsilon_{\tilde{U}}$ from LES is presented in Figure 17 and compared with the predictions by the surrogate model of $\epsilon_{\tilde{U}}$. Both of them show a similar evolution trend while deviations between them can reach at most 12%. The minimum is located at 0.11 according to LES and at 0.12 based on the prediction of surrogate model. In this case we give more credit to LES results and the value chosen is 0.11 for C_s , though 0.12 would give almost the same result.

5 CONCLUSIONS AND FUTURE WORK

In this work, a UQ-CFD methodology was presented and applied to the LES of a turbulent pipe flow. The methodology consists of evaluating uncertainties from parameters of models used. UQ analysis is based on surrogate models of QoIs from LES, thus reducing the computational cost generated by

Figure 16: \tilde{U} obtained using LESFigure 17: Comparison of $\epsilon_{\tilde{U}}$ from LES and surrogate model

numerous LES in the application of UQ techniques. Different capabilities of the developed methodology are illustrated, including sensitivity analysis, data calibration and uncertainty propagation.

The analysis shows that parameters of the wall model are more critical in the pipe simulation, while the impact of the parameter of the SGS model increases near the wall. With the help of the data calibration, uncertainties on parameters are largely reduced as well as those on QoIs $\tilde{U}(r)$. A strong correlation is found between parameters of the wall-model, which is intrinsic to the model formulation. Following the UQ analysis, an optimal set of parameters is proposed which allows to minimize the errors on the velocity profile compared to the reference DNS data.

It is worth emphasizing that the proposed methodology, which combines Latin Hypercube sampling, surrogate modeling, sensitivity analysis and Bayesian data calibration is general and can be applied to any UQ problem involving complex computer codes. The application of such a methodology on a relatively simple case also allows us to anticipate difficulties when studying more complex cases.

In the future work, the application of current methodology on internal combustion engine simulation is envisaged, however some challenges stand out :

- In this study, a single LES of a pipe flow demands a runtime of 7 hours on 36 CPUs, in total around 250 CPU.hours. 400 experiments are used for building surrogate models, resulting in a total computational cost of 10^5 CPU.hours. For more complex engine simulations, a single engine cycle requires much more computational resource of about 10^4 CPU.hours, which makes the current methodology too expensive to use, even only for surrogate modeling.
- Unlike the pipe flow which is statistical stationary, in-cylinder engine flow is totally transient and presents variabilities between different cycles. Thus, QoIs extracted from a single cycle may not be representative of the global characteristics of the flow and values obtained from a certain number of cycles is preferred, which again increases the computational cost of a single experiment.

In our next studies we'd like to integrate an adaptive sampling strategy coupled with surrogate modeling with which DOE is not generated once but updated consecutively by adding critical samples to improve the quality of surrogate models efficiently. Also, qualitative studies will be carried out to investigate the main uncertainty sources in engine simulations and define quantifiable QoIs for UQ analysis.

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