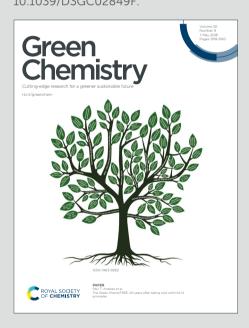




Cutting-edge research for a greener sustainable future

Accepted Manuscript

This article can be cited before page numbers have been issued, to do this please use: S. Aslam, S. Rani, K. Lal, M. Fatima, T. Hardwick, B. Shirinfar and N. Ahmed, *Green Chem.*, 2023, DOI: 10.1039/D3GC02849F.



This is an Accepted Manuscript, which has been through the Royal Society of Chemistry peer review process and has been accepted for publication.

Accepted Manuscripts are published online shortly after acceptance, before technical editing, formatting and proof reading. Using this free service, authors can make their results available to the community, in citable form, before we publish the edited article. We will replace this Accepted Manuscript with the edited and formatted Advance Article as soon as it is available.

You can find more information about Accepted Manuscripts in the <u>Information for Authors</u>.

Please note that technical editing may introduce minor changes to the text and/or graphics, which may alter content. The journal's standard <u>Terms & Conditions</u> and the <u>Ethical guidelines</u> still apply. In no event shall the Royal Society of Chemistry be held responsible for any errors or omissions in this Accepted Manuscript or any consequences arising from the use of any information it contains.



Electrochemical Hydrogen Production: Sustainable Hydrogen Economy

Samina Aslam¹, Sadia Rani¹, Kiran Lal¹, Miraj Fatima¹, Tomas Hardwick², Bahareh Shirinfar³ and Nisar Ahmed²'*

¹Department of Chemistry, The Women University Multan, Multan60000, Pakistan

Keywords: Electrolysis, hydrogen evolution, renewable energy, efficiency, sustainability

Abstract

The development of sustainable energy technologies has received considerable attention to meet increasing global energy demands and to realise organisational goals (e.g., United Nations, the Paris agreement) of carbon neutrality. Hydrogen is a promising alternative energy source to replace fossil fuels and mitigate corresponding environmental issues. An aspiring method to produce hydrogen is to direct energy from intermittent renewable energy sources for water electrolysis. However, a major obstacle to practically achieve hydrogen storage is the future investment costs of water electrolysis due the energy intensive nature of the reaction. In this study, we present an overview of current research interests that produce hydrogen, including different types of water electrolysis such as high temperature, low temperature, nuclear-driven, solar-powered, wind powered, and grid connected water electrolysis. Electrolysis using organic fuels and hydrogen production as a by-product of various electrolytic methods are also briefly discussed. At the end, we demonstrate economy, sustainability, and challenges of sustainable hydrogen production reporting since 2005 onwards.

Introduction

It is well known that the continued burning of fossil fuels releases greenhouse gases into the atmosphere, which poses a major threat to the environment and leads to changes in climate.¹ Additionally, infrastructure of a country that is dependent on the importation of foreign fuel sources will display vulnerability as a result of the increase in conventional fuel costs that have been forced by the rising energy demand. Future energy sources would ideally be carbon-free and

²School of Chemistry, Cardiff University, United Kingdom

³Department of Chemistry, University of Bath, BA2 7AY, Bath, United Kingdom.

^{*}Corresponding Author: nisarhej@gmail.com, AhmedN14@cardiff.ac.uk

renewable in order to combat climate change on a long-term basis and reduce our reliance on foreign oil.^{2, 3}

Hydrogen can be employed in future energy frameworks since it is a carbon-free alternative energy source with several benefits, such as environmental friendliness and high energy density. Clean and sustainable energy is produced from various energy sources all over globe usinghydrogen derived from renewable resources.⁴

H₂ has the highest specific energy of any fuel now in use, with 33.31 kWh/kg. By comparison, gasoline has a specific energy of 12.89 kWh/kg and lithium-ion batteries have a specific energy of 0.1–0.2 kWh/kg.^{5, 6} Due to the high energy density, 5 kg of H₂ is sufficient to propel a typical passenger vehicle 500 km in less than 5 minutes.⁷ This is the key advantage over battery-powered cars, which require heavier and larger batteries to travel the same distance and have longer refueling intervals.⁸

To date there are a variety of sustainable and high-purity processes for electrolysis-based hydrogen production. There is much interest in, and funding, for this field of study, as seen by the increase in the number of scientific publications on the subject of hydrogen synthesis by the electrochemical splitting of water. In addition to being manufactured as a fuel for transportation, hydrogen can also be produced as a feedstock for the chemical industry and as a solution to address the intermittent nature of renewable energy sources such as wind and solar energy. The existence of economically viable methods for sustainable hydrogen production is essential in making this vision a reality. Today, however, with around 96% of the world's hydrogen generation (mostly for ammonia production) relying on the steam reforming of fossil fuels, this is not the case. Around 60 million tonnes of hydrogen are produced each year on a global scale. Nearly half of this is created by the steam reforming of natural gas, 29% through the reforming of oil, and 17% through the gasification of coal, all of which emit significant amounts of greenhouse gases. Additionally, water electrolysis produces around 4% of the hydrogen. At present, annual hydrogen consumption growth is 6%.

There are numerous ways to make hydrogen which have traditionally relied upon electro-, and thermochemical processes, in addition to biochemical methods that occur via fermentation, biophotolysis, or biological metabolic pathways. Electrochemistry involves the splitting of water

into molecular hydrogen and oxygen, primarily through water electrolysis. Through reforming, pyrolysis, and gasification reactions of biomass and fossil fuels, hydrogen is produced thermochemically (carbonaceous fuels).¹³ Notwithstanding this, thermochemical processes, photobiological water splitting, and biomass fermentation are a few of the potential methodologies that are being researched in order to produce hydrogen sustainably.¹⁴ The need for sustainable energy sources is becoming increasingly important due to the rising global demand for energy and the need to reduce carbon emissions and ecological pollution. The current favourable (lower cost) generation of hydrogen from fossil fuels, in comparison to alternative technologies based on renewables, is the biggest obstacle to the introduction of renewable routes to hydrogen production. Other processing techniques, such as the gasification of biomass or the splitting of water using external energy sources like sunlight, have the potential to utilise more sustainable methods orfeedstock's, despite the majority of hydrogen generation coming from unsustainable routes using carbon-based fuels. In light of this current less-than-optimal nature of hydrogen generation, more efficient alternative routes must be developed in conjunction to other energy supply channels. Many renewable-based technologies have efficiency restrictions, thus in practice, a variety of technologies will need to be made commercially viable in order to meet the demand for a significant increase in sustainable hydrogen generation.¹⁵ When compared to the usage of fossil fuels and biofuels, hydrogen offers some advantages that could be deemed favorable. ¹⁶ **Table 1** demonstrates brief summary of principles of various high performance hydrogen production methods.

In this article, we give an overview of the several types of water electrolysis being researched today, including solar-powered, grid-connected, high temperature, low temperature, nuclear-assisted and wind-powered water electrolysis. Hydrogen production as a by-product of several electrolytic processes and electrolysis utilizing organic fuels are also slightly explored. We conclude by highlighting the cost, sustainability, and difficulties of sustainable hydrogen production.

Table 1: Summary of principles of Green Hydrogen production methods¹⁷

Hydrogen production methods		Material resources	Process driving energy	Brief description
Thermolysis		Water	Si.	Steam is heated to over 2500 K, where water molecules thermally disintegrate.
	Gasification	Biomass		Syngas is produced from biomass, and H ₂ is removed.
	Water			Chemical reactions are carried out,
Thermochemical	splitting	Water		whether or not they involve redox reactions.
processes	H ₂ S splitting	H_2S	Thermal energy	Cyclical processes to break the hydrogen sulfide molecule
	Reforming	Biofuels		Conversion of liquid biofuels into hydrogen
	Biomass	Biomass		Conversion of biomass to hydrogen by
	conversion			thermocatalysis
Thermocatalysis	H_2S			Thermo-catalytic H ₂ S is broken down
	cracking	H_2S		from seawater or other industrial processes.
				Syngas is created from coal, and
Coal gasification		Water		subsequently H_2 is removed and CO_2 is separated and sequestered (using electricity).
		Fossil		With CO ₂ capture and isolation, fossil
Fossil fuels reform	ning	fuels		hydrocarbons are transformed to H_2 (electricity used).
			Electrical +	Splits water in solid oxide electrolyte cells
High temperature	electrolysis	Water	thermal	using both an electrical and thermal source.
Thermo-catalytic	fossil fuels	Fossil		Fossil hydrocarbons are split into H ₂ and
cracking		fuels		CO ₂ via a thermo-catalytic process, while
				CO ₂ is separated or sequestered to make

Hybrid thermochemical cycles	Water		the method green. Utilize thermal and electrical energy to cycle through chemical reactions, which will ultimately lead to the splitting of water.
Plasma arc decomposition	Natural gas	Electrical energy	Hydrogen and carbon soot are formed when cleaned natural gas (methane) is pushed through an electrically generated plasma arc.
Electrolysis	Water		An electrochemical process that generates a direct current leads water to decompose into oxygen and hydrogen gas.
Dark fermentation	Biomass	Biochemical energy	Without light, anaerobic fermentation
Thermophilic digestion	Biomass	Biochemical + thermal	Uses thermal energy helped by biomass digestion to heat at low grade temperature.
Photo-electro-chemical method	Water		The water electrolysis process is powered by photovoltaic electricity produced by a hybrid cell.
PV-electrolysis	Water		Electricity from solar panels powers the electrolyzer.
Bio-photolysis	Water	Photonic energy	Utilizing cyanobacterial-based biological systems, hydrogen is produced under controlled conditions.
Photo-catalysis	Water		Hydrogen is produced from water using sophisticated homogeneous catalysts or molecules with photo-initiated electron
Photo-fermentation	Biomass		collecting. By exposing the fermentation process to light, it is facilitated.

			Uses bacteria and other microorganisms to
	Biomass,		photogenerate hydrogen.
Bio-photolysis	Water		
		Photonic +	
A 4° 6° - 1 1 4 4 1 1	D:	biochemical	To simulate abote continuing and another
Artificial photosynthesis	Biomass,		To simulate photosynthesis and produce
	water		H ₂ , chemically modified molecules and
			related systems are used.
Photo-electrolysis	Water	Electrical +	Photo-electrodes and external source of
		photonic	electricity are required.

1. Electrochemical Production of Hydrogen

As the most prevalent element in the universe, hydrogen is easily accessible in the form of biomass from plants, water, hydrocarbons, and other organic substances. Hydrogen is currently produced more for use as a chemical or reducing agent than as a fuel. As energy carrier or energy vector rather than an energy source, hydrogen produced from renewable resources can offer an energy pathway that is both clean and sustainable. Fig 1 gives the certain primary energy sources and their routs to hydrogen production. 10

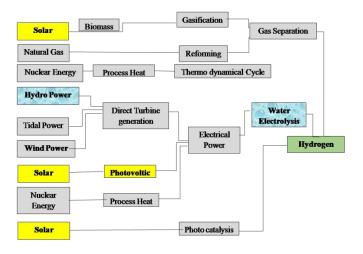


Fig 1: The primary energy sources considered and their routs to hydrogen. Reproduced from ref.¹⁰ with permission from [Elsevier], copyright [2005].

To fulfil its role in the future, hydrogen production must meet three key criteria:

This article is licensed under a Creative Commons Attribution-NonCommercial 3.0 Unported Licence

Open Access Article. Published on 19 October 2023. Downloaded on 10/24/2023 3:00:04 PM.

- ii. It ought to make use of plentiful and renewable feedstock's;
- iii. High purity hydrogen must be produced because contaminants are hazardous in most fuel cell and other applications. High purity hydrogen must be produced because contaminants are hazardous in most fuel cell and other applications.

Hydrogen may only be regarded as sustainable if both the process's feedstock and the energy source for its electrical input are renewable.²⁸ The options for producing hydrogen sustainably are elaborated in this study. Fuel cells that use hydrogen to produce energy can be employed with ease. Additionally, hydrogen has a high energy yield of 122 kJ/g, which is 2.75 times higher than fuels derived from hydrocarbons.²⁹ As a technical and policy problem, the use of hydrogen as a fuel for mobile and stationary applications is getting a lot of positive attention.³⁰ The estimated total annual hydrogen consumption for the entire planet is 400–500 billion Nm³.³¹ The current use of hydrogen accounts for 3% of global energy consumption, with a growth rate of 5–10% each year.³² There are numerous ways to manufacture hydrogen, and **Table 2** lists them along with their benefits and drawbacks for producing hydrogen energy.^{21, 24-27} Electricity is used in electrolysis to divide water molecules into hydrogen and oxygen, and the price of electricity is a major factor in the cost of producing H₂ energy.^{21, 33, 34}

Table 2: Hydrogen production from various sources and related mechanisms, efficiencies, costs as well as advantages/ disadvantages.^{21, 24-27}

ACommercial 3.0 Underted Lie	Mechanism	Benefits	Drawbacks	Hydrogen cost (\$ kg ⁻¹)	Efficiency (%)	References
SCORE STATE OF THE	$2H_2O \rightarrow 2H_2 + O_2$	Proven technology. Zero emission. Only by-product is O ₂ . Existing infrastructure already developed.	Storage problems. Applicable only to special purposes. Transportation issues.	10~23	40~60	19, 20
Access Article: Tubusing on 19 October 2023. Downtoaded on 19	Biomass + H_2O + Air \rightarrow H_2 + CO_2	Dependent on renewable sources. Other useful products can be obtained such as adhesives, polymers, fertilizers. Less expensive.	Inefficient when compared to fossil fuels. Not entirely a clean source because of methane gas produced as a by-product. potential contribution to deforestation.	2.05	35~50	so Cepted Man 12
Steam Enethane Efeforming	Biogas + steam \rightarrow H ₂ + CO ₂	Existing infrastructure. Most developed of these technologies.	Unstable supply. Geopolitical tension. Pollution (CO, CO ₂).	2.27	74~85	20
uclear energy	$C_1H_2(Synthetic$ crude) + $2H_2O$ +nuclear heat \rightarrow $CO_2 + 3H_2$	Less carbon production.	Disposal of radioactive waste. Mining and processing of uranium. Potential for accidents.	4~7	45~50	22
Gasification of coal	+ 2H ₂	Less CO ₂ emitted than conventional fossil fuel burning. Syngas can be easily collected and used to produce carbon neutral fuels.	production of heavy oils, petroleum and coke can occur. Large amounts of CO ₂	1.48	60~75	22, 23

In **Table 3**, the environmental effects of the various electrolysis procedures are described together with the current and projected costs of producing hydrogen through electrolysis utilising various electricity sources.^{34, 35} **Table 3** shows that the most dependable and economically efficient way to currently produce hydrogen is through electrolysis utilising hydropower, although nuclear

power is looking to capitalise in the future. Despite being a viable replacement for fossil fuels, hydrogen still faces several difficulties. Due to hydrogen's inability to liquefy at room temperature, these difficulties mostly relate to the high cost of production and the difficulty in storage. 16, 35, 36

Table 3: Comparison of various electricity sources for water electrolysis ^{34, 35}

Electricity source	Present cost (\$ kg ⁻¹)	Future cost (\$ kg ⁻¹)	CO ₂ emission (kg CO ₂ kg ⁻¹ H ₂)	Efficiency (%)
Hydro	1.4	3~4	0	25
Wind	7~11	3~4	0	21
Nuclear	4.15~7	2.45~2.63	0	45
Solar	10~30	3~4	0	20

Using a strategy based on distinct colours, hydrogen generating technologies are increasingly being stated. ³⁷⁻³⁹ Grey (or brown/black) hydrogen is created by fossil fuels (mostly coal and natural gas), which results in the release of carbon dioxide.²⁰ Blue hydrogen prevents the majority of the process's GHG emissions by combining grey hydrogen and carbon capture and storage (CCS). Natural gas is converted into blue hydrogen by the steam reforming process. In this process, natural gas is broken down into hydrogen (H₂) and carbon dioxide (CO₂), with some of the generated CO₂ unable to be captured, while the remaining CO₂ is captured (85%–95%) and stored underground using commercial carbon capture and storage techniques. Leakage can still have a harmful impact on ecology and the climate, and the long-term effects of storage are undetermined. 40 Solid carbon in the form of carbon nanotubes or filamentous carbon is a by-product of the pyrolysis of methane to produce turquoise hydrogen. 41 Green hydrogen is manufactured by electrolysers powered by renewable electricity. It can also be generated via alternative bioenergy-based processes like biomethane reforming or solid biomass gasification. 42 Through atomic current electrolysis, purple hydrogen can be produced. Incorporating a hydrogen producing facility could lessen the need to shut down nuclear power facilities.⁴³ The term "yellow hydrogen" is occasionally used in literature to refer to purple/ pink hydrogen. However, the more typical definition of yellow hydrogen for grid-powered electrolysis is employed. Finally, white hydrogen is hydrogen from its natural form or as a by-product of industrial processes.³⁷

Since its invention in the late 1920s, electrolysis has been used to produce pure hydrogen commercially. In this case, water is separated into hydrogen and oxygen using external electricity. By the 1960s industrialised hydrogen production had switched to options fuelled by fossil fuels which have continued to be the primary source of energy and raw materials for the manufacture of hydrogen. Only 4% of the total hydrogen supply in the world is now produced by electrolysis. Numerous hydrogen production techniques, including electrolysis, have been thoroughly researched from an economic, environmental, technological, and social standpoint in the literature. 9, 27, 42, 45-58

The electrolyser is the fundamental part of an electrolysis process for producing hydrogen (can be connected either in parallel or in series). The by-product gases, typically hydrogen and oxygen, are often cooled and compressed before being stored for multiple end uses. Since oxygen is typically not a desired result in electrolysis procedures, it is usually immediately released into the environment rather than entering storage. Additionally, the water supply to the electrolyser needs to be adequately treated to remove contaminants and, by extension, any possibility for unintended side reactions. Moreover, due to the absence of moving parts in most electrolysers, routine maintenance is not necessary. The silent operation and modular design of electrolysers make them suitable for distributing an energy supply to residential, commercial, and industrial units. To reduce the costs of electrolyser manufacturing, distribution, and installation, considerable technological and material advancements are needed to coincide with efficient function at ambient conditions.¹³ Different technologies have been compared for their energy efficacy in producing hydrogen (**Fig 2**).¹⁹

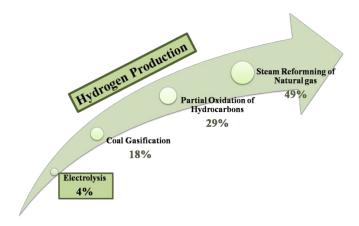


Fig 2: Different methods of hydrogen production. Reproduced from ref.¹⁹ with permission from [Elsevier], copyright [2022].

Currently, electrolysis creates pure hydrogen for use in the food, pharmaceutical, electronics, and other industries⁵⁹⁻⁶² and is being studied as a potential technique to create hydrogen for use as a fuel.⁶³ Potentially, electrolysis can offer a clean and sustainable supply of chemical energy when combined with a renewable energy source. In other cases, electrolysis can benefit from off-peak energy to lower the cost of electricity. Two commercial electrolyser technologies are alkaline and solid polymer electrolysers, while alkaline polymer, solid oxide, and molten carbonate are three technologies that are currently being researched and developed.⁶⁴

Among other operating factors, electrolysers can be categorised based on their operating temperature. The most common systems use polymer electrolyte membrane (PEM) and alkaline technologies in low-temperature electrolysers, sometimes referred to as "water electrolysers", while molten carbonate electrolysis (MCE) cells and solid oxide electrolysis(SOE) cells are examples of high-temperature electrolysers, also referred to as "steam electrolysers". Due to two primary factors, an increase in the electrolysis temperature is of tremendous interest. Firstly, this is because high-temperature technologies often require less energy than low-temperature ones. In fact, a portion of the electrical energy required to break down the water molecule can be replaced by heat as the temperature rises. Secondly, because of their internal fuel processing capability, which is improved by higher operating temperatures and the presence of catalysts, they can process hydrocarbon fuels without experiencing severe degradation difficulties. Since losses, including ohmic losses, are reduced at higher temperatures. Hydrogen may be produced with very low

specific electrical consumption of 3–4 kWh/Nm³ by high-efficiency upgrading of hydrocarbon streams.⁶⁷

1.2. Electrocatalysts for Hydrogen Production

Electrocatalysts are required for electrochemical energy conversion and storage techniques in order to create environmentally responsible and long-lasting energy systems. Systems that use electrochemistry for energy conversion and storage often employ a wide variety of electrochemical processes; they generate less carbon dioxide and have high energy densities. The effectiveness and affordability of the electrocatalyst are crucial for its broad application. The use of electrocatalysts increases the electrolysis system's energy efficiency. We selected a few examples to highlight many sorts of electrocatalysts from the many electrocatalyst examples that are accessible. Many compounds based on transition metals have proven to be effective electrocatalysts.^{9, 27, 45, 55, 57, 68-95}

Due to their powerful electrocatalytic activity, transition metal compounds (such as carbide, oxide, sulfide, phosphide, selenide, and others) are among the many electrocatalyst candidates being researched. The workings of different electrocatalysts differ. Because they facilitate the conversion of reaction intermediates and lower resistance, electrocatalysts are essential for increasing reaction speeds. Noble metals are the most complex electrocatalysts for OER (Ir/Ru oxide), HER (Pt), and ORR (Pt), but due to their high cost and scarcity, they are not frequently utilized in industry. Even at relatively low platinum loadings, a number of commercial electrodes constructed from Pt(Mo₂C)-produced catalysts exhibit significant catalytic activity for the hydrogen evolution reaction (HER) in 0.5 M sulfuric acid solution.⁷³ Commercial electrodes made of Ni and Ti mesh function well, offer superior cathode materials, and cost less than electrodes made of Pt.⁷⁴ Other materials offer the best electrode materials for general application since they are less expensive than Pt-based electrodes and have good performance. Of course, the cost of the electrodes must come next. They can be made of costly and affordable materials, corrosion-resistant metals, and alloys, including noble metals.

The components used for manufacturing the electrodes used in water in general, but particularly in seawater electrolysis, must adhere to precise specifications. Both the most extensively researched hydrogen evolution reaction (HER) and the less well-known oxygen evolution reaction

(OER) must occur at the electrodes in seawater, hence the electrodes must have electrocatalytic qualities. On the electrolysis cell, this will lessen polarizations and explicit voltage losses. The findings of investigations on appropriate seawater electrocatalysts for HER recently employed in the electrolysis process are shown in **Table 4**.

Table 4: A few examples on electrocatalysts for hydrogen production⁹

Electrocatalysts	Stability, h	References
$Ni-N_3$	14	72
Co-Se	12	96
CoP-WP/rGO	30	97
FeOOH/ β-Ni–Co-OH	378	98
NiMoS	100	75
MFC-N,O doped C	76	86
Co/GCFs	10-20	78
MNiNS, Ni/Pt-C, Ni/Ir-C	12	99
FeCo-Ni2P, MIL-FeCoNi	100	85
Pt-NiFe PBA	12	77
NiCo@C	60-140	100
MXene, carbide	225	94
Ni2P-FeP	90	81

2. Water Electrolysis

This approach makes reference to the earliest technique for creating hydrogen, which dates to the 19th century. Although abundant, renewable energy is sometimes unreliable and intermittent. The need to store energy for times when the sun is not beaming and the wind is not blowing will increase as our reliance on renewable energy increases. Utilising renewable energy (as and when it becomes available) to split water into hydrogen and oxygen in accordance with equation 1 is one of the more interesting methods for storing this energy.

A carbon-neutral fuel production and consumption cycle can be created by storing the hydrogen created by the reaction in **equation 1** and then oxidising it (by burning in air or in a fuel cell) to release energy and regenerate water. The overall reaction is shown below:

$$H_2O + electricity \rightarrow H_2 + \frac{1}{2}O_2$$
 (1)

At room temperature and pressure, the reaction in equation 1 is a thermodynamically upstream process and needs an energy input of 286 kJmol⁻¹. This conversion is thought to be best accomplished via electrochemical methods, which just need inputs of water and voltage to make hydrogen. ¹⁰⁴ According to the **equation 2**, water is oxidised at the anode when the environment is acidic.

$$2H_2O \rightarrow O_2 + 4e^- + 4H^+$$
 (2)

These protons cross into the cathode compartment (to complete the electrochemical circuit), the electrons move through the external circuit. The hydrogen evolution reaction (HER), which combines the protons and electrons at the cathode, follows:

$$4e^- + 4H^+ \rightarrow 2H_2$$
 (3)

The minimal theoretical voltage needed to drive the OER and HER (to split water) is 1.23V at ambient temperature. The reactions must have additional energy, or activation energy, in order to occur at noteworthy rates. The amount of activation energy required increases with the rate of water splitting (measured as charge flowing per unit area of electrode per unit time, or "current density"). The necessity for potential bias above the 1.23V minimum results from the increased energy. The finest electrocatalysts for acidic environments (where protons serve as the electrochemical charge carriers, as shown in the figure below) are precious metals (platinum at the cathode and IrO2 or RuO2 at the anode). First row transition metals (and their alloys) and oxides provide effective HER and OER catalysts, respectively, when the HER and OER proceed under the basic conditions stated in the equations below. 104

Basic HER:
$$4H_2O + 4e^- \rightarrow 2H_2 + 4OH^-$$
 (4)

Basic OER:
$$4OH^- \rightarrow O_2 + 2H_2O + 4e^-$$
 (5)

The oxygen evolution reaction (OER) and hydrogen evolution reaction (HER) are the two main processes that make up overall water electrolysis. Both of these reactions require effective electrocatalysts 105-107 to speed up their slow kinetics for high energy efficiency. 104, 108-110 Transition metal-based electrocatalysts play an important role for clean energy. 111, 112 The development of non-precious OER/HER electrocatalysts as substitutes for Pt/C and Ir/Ru based catalysts has made

significant progress in recent years. ^{113, 114} **Fig 3** below depicts a typical electrolysis cell for splitting water.

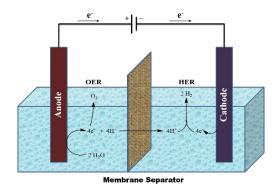


Fig 3: Electrolysis cell for splitting water. Reproduced from ref.¹⁰⁴ with permission from [Nature Publishing Group UK London], copyright [2017].

About 1×10⁻⁶ S/m is the electrical conductivity of pure water, making it a poor conductor of electric currents. Under these conditions, hydrogen and oxygen production would require very high voltages. To make water more conductive, salts, acids, or bases are typically added. Acidic and alkaline solutions have higher electrical conductivities than neutral solutions because hydrogen ions (H⁺) and hydroxyl ions (HO⁻) have a greater degree of mobility in these environments. Despite the fact that acidic solutions are more conductive than alkaline solutions, the corrosion of steel-based metallic components leads to a rise in the material consumption of the electrodes, which results in process losses. Due to the formation of carbonates under the effect of carbon dioxide in the air, which results in a 75% reduction in initial conductivity, the electrical conductivity of alkaline electrolytes diminishes with time.⁹

As a sustainable approach, water electrolysis technology has been developed to produce high-purity hydrogen, called green hydrogen. A voltage is applied to the cells during water electrolysis, and a DC current travels between two electrodes while in contact with an ionic conducting medium, producing hydrogen and oxygen from the breakdown of water (**Fig 4**).²⁰

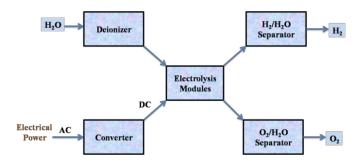


Fig 4: Flow diagram of the water electrolysis process. Reproduced from ref.²⁰ with permission from [Elsevier], copyright [2017].

The best way for splitting water is electrolysis, which is a solidified and famous process.²⁰ However, because of how endothermic the process is, electricity is used to supply the needed energy input.¹¹⁵ In practise, the electrolysis of water achieves an energetic efficiency of 50–70% (chemical energy obtained per electrical energy provided).⁴

Since high purity water supplies are necessary for all commercially available water electrolysers, a low system efficiency of 70% and high cost limit the applicability of water electrolysis. 116-118 In many places, especially in hot, arid locations, freshwater has historically been a rare resource. Equipment for water purification and desalination is required while building an electrolytic water system in order to pre-treat saline and low-grade water. 119, 120 The flow of input-fluid and outflow-air streams, gas regulators, and thermal management devices are all complicated setups that distinguish practical electrolysers from basic laboratory systems. Even before factoring in related investments in transportation and maintenance, the deployment of more water purification devices will eventually come at a prohibitive cost. Direct use of saline seawater in water electrolysis systems can be a feasible and practical strategy for coastal dry zones and offshore large-scale hydrogen outputs when cost reduction is taken into account. The economic efficiency of purification/desalination can be significantly increased by removing pre-treatment systems. For the electrolysis of water and seawater to produce hydrogen, solar energy, geothermal energy, wind, micro-hydropower, and wave energy are all appropriate sources of energy (Fig 5).

This article is licensed under a Creative Commons Attribution-NonCommercial 3.0 Unported Licence

Open Access Article. Published on 19 October 2023. Downloaded on 10/24/2023 3:00:04 PM.

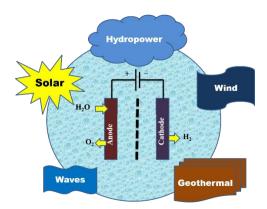


Fig 5: Renewable sources of energy for hydrogen production from seawater electrolysis. Reproduced from ref.⁹ with permission from [MDPI], copyright [2022].

The market for hybrid renewable energy systems has grown significantly as a result of the year-round fluctuations in the availability of renewable energy sources like solar, wind, small hydro, geothermal, and ocean power. Numerous research on the architecture, operation, dependability, and optimisation of hybrid renewable energy have been published recently in response to the rise in demand. The key renewable energy sources listed in **Table 5** can be used to electrolyse seawater in a sustainable manner.^{49, 75, 119-142}

Table 5: Main renewable sources of energy that could be sustainably used for seawater electrolysis.⁹

Type of Renewable Source	References
Wave energy	122
Geothermal Energy	122, 124, 142
Wind energy	122, 124, 125, 128, 132, 135, 137, 139
Hybrid renewable energy	121, 124, 126, 130, 134-142
Solar energy	9, 59, 75, 121, 123-125, 127, 129-132, 134, 136-139
Microhydropower	139

Alkaline water electrolysis, proton exchange membrane (PEM) water electrolysis, and solid oxide water electrolysis (SOEC) can produce hydrogen when different electrolytes are used. 143 Key features of these techniques are described in **Table 6**.

Table 6: Technical features of common water electrolysis methods. 144

Features	Alkaline	AEM	PEM	Solid Oxide
Anode reaction	$2OH^- \rightarrow H_2O +$	$2OH^- \rightarrow H_2O + \frac{1}{2}$	$H_2O \rightarrow 2H^+ + \frac{1}{2}O_2 +$	$O^{2-} \rightarrow \frac{1}{2} O_2 + 2e^-$
	$^{1}/_{2}$ O ₂ + 2e ⁻	$O_2 + 2e^-$	$2e^{-}$	

Cathode Reaction	$2H_2O + 2e^- \rightarrow$ $H_2 + 2OH^-$	$2H_2O + 2e^- \rightarrow H_2 + 2OH^-$	$2H^+ + 2e^- \rightarrow H_2$	$H_2O + 2e^- \rightarrow H_2 + O^{2-}$
Overall cell	$H_2O \rightarrow H_2 + \frac{1}{2}$ O_2	$H_2O \rightarrow H_2 + \frac{1}{2}O_2$	$H_2O \rightarrow H_2 + \frac{1}{2}O_2$	$H_2O \rightarrow H_2 + \frac{1}{2} O_2$
Operating temperature	70–90°C	60–40°C	50-80°C	700–850°C
Efficiency	50-78%	57–59%	50-83%	89% (laboratory)
Electrolyte	Electrolyte KOH/NaOH (5M)	DVB polymer support with 1 M KOH/NaOH	Solid polymer electrolyte (PFSA)	Yttria stabilized Zirconia (YSZ)
Electrode/ Catalyst (Hydrogen side)	Nickel coated perforated stainless steel	Nickel	Iridium oxide	Ni/YSZ
Electrode/ Catalyst (Oxygen side)	Nickel coated perforated stainless steel	Nickel or Nickel alloys (NiFeCo)	Platinum carbon	Perovskites (LSCF, LSM) (La,Sr,Co,FE) (La,Sr,Mn)
Cell Pressure	<30 bar	<35 bar	<70 bar	1 bar
Separator	Asbestos/Zirfon /Ni	Fumatech	Nafion®	Solid electrolyte YSZ
Electrode area	10,000–30,000 cm ²	<300 cm ²	1500 cm ²	200 cm ²
Lifetime (stack) Gas Diffusion layer	60,000 h Nickel mesh	>30,000 h Nickel foam/carbon cloth	50,000–80,000 h Titanium mesh/carbon cloth	20,000 h Nickel mesh/foam
Capital costs (stack) minimum 1 MW	US \$270/kW	Unknown	US \$400/kW	>US \$2000/kW
Capital costs (stack) minimum 10 MW	US \$500– 1000/kW	Unknown	US \$700–1400/kW	Unknown
Bipolar Plates	Stainless steel/Nickel coated stainless steel	Stainless steel/Nickel coated stainless steel	Platinum/Gold-coated Titanium or Titanium	Cobalt coated stainless steel
H ₂ purity	99.5–99.9998%	99.9–99.9999%	99.9–99.9999%	99.9%
Development status	Mature	R & D	Commercialised	R&D
Nominal current density	0.2–0.8 A/cm ²	0.2–2 A/cm ²	1–2 A/cm ²	0.3–1 A/cm ²

Voltage range 1.4–3 V 1.4-2.0 V 1.4-2.5 V 1.0-1.5 V (limits)

2.1. **High Temperature Water Electrolysis**

This type of water electrolysis consists of following types:

2.1.1. Molten Carbonate Electrolysis (MCE)

MCE and SOE are the most effective yet the least developed. Numerous researchers have examined electrolysis in molten carbonate salts, primarily concentrating on the electrolytic reduction of carbonate melts or carbon dioxide into solid carbon or gaseous carbon monoxide. 145-¹⁵⁵The molten carbonate electrolyte suspended in a porous and chemically inert ceramic matrix underlies the molten carbon fuel cells (MCFC) technology, from which MCEs are formed. The electrolysers working principle is the opposite of that of the fuel cells, the difference between the MCE cells and MCFC is in the direction of the redox reaction. The materials used to assemble the components of the MCE cells are the same as those used to assemble the MCFCs, with the exception that the cathode consists of porous nickel alloyed with Cr and/ or Al, and the anode is from of porous lithiated nickel oxide (NiO). The lithium, potassium, and/or sodium carbonate (Li₂CO₃, K₂CO₃, and Na₂CO₃) combination is used as electrolyte. Operating with a liquid carbonate electrolyte is possible when the temperature is between 620 and 680°C. Only a few MCE-specific research are reported in the literature. However, despite being at a highly advanced level of research, MCFC technology is the only one of the fuel cell technologies to have produced power plants with several megawatts of output. The functional layout of a Molten Carbonate Electrolyser Cell (MCEC) is shown in **Fig 6**. ¹⁵⁶ Hydrogen electrode reactions are:

$$H_2O + CO_2 + 2e^- \rightarrow CO_3^{2-} + H_2$$
 (6)

$$2\text{CO}_2 + 2\text{e}^- \rightarrow \text{CO}_3^{2-} + \text{CO} \tag{7}$$

In reaction (vi), steam is electrolysed in an MCE while in reaction (vii), carbon dioxide undergoes an electrochemical reaction to form carbon monoxide. The latter is slower and is not predicted to happen in the hydrogen electrode, according to literature reports. 157 It is anticipated that carbon monoxide will be produced through an equilibrium shift because of the operating temperature and **Green Chemistry Accepted Manuscript**

the presence of nickel catalyst in the fuel electrode. Since steam and carbon dioxide are the only accessible reactants in this situation, the reaction is known as the reverse water gas shift. The local condition indicates that all species are present and the reaction has reached thermodynamic equilibrium. The following is the reaction:

$$CO_2 + H_2 \leftrightarrow H_2O + CO$$
 (8)

Theoretically, both electrochemical (vii) and chemical (viii) reactions can result in the production of carbon monoxide. The interaction of reactions (vii) and (viii) results in reaction (vi), which combines the reactions of carbon dioxide and steam. The following describes an oxygen electrode reaction:

$$CO_3^{2-} \rightarrow CO_2 + \frac{1}{2}O_2 + 2e^-$$
 (9)

As an intake reactant, oxygen gas is not needed. Carbon dioxide and oxygen are produced via the OER. The entire reaction between the two electrodes is the breakdown of water into hydrogen and oxygen:

$$H_2O \to H_2 + \frac{1}{2}O_2$$
 (10)

Carbon dioxide moves from the hydrogen electrode to the oxygen electrode during the procedure. This indicates that both CO₂ and steam must be supplied to the electrode. A MCEC differs from a conventional electrolyser in that carbon dioxide is supplied to the hydrogen electrode and produced at the oxygen electrode. The hydrogen electrode contains carbon dioxide, which causes a chemical or electrochemical reaction that also produces carbon monoxide.¹⁵⁸

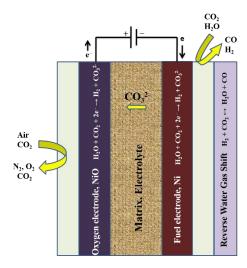


Fig 6: Working principle of a molten carbonate electrolysis (MCE) cell. Reproduced from ref. with permission from [Elsevier], copyright [2018].

In addition to transporting the carbonate ions between the electrodes and separating the fuel and oxidant gases, the electrolyte is retained in a porous matrix, typically constructed of γ -LiAlO₂.⁶⁷ However, because carbon dioxide is involved and the product stream from the electrolyser contains both hydrogen and carbon dioxide, there is a significant practical issue with the operation of an MCE cell, necessitating gas separation for the production of pure hydrogen and recycling of carbon dioxide to the cell. In order to produce syngas (a combination of CO and H₂) through coelectrolysis of water and carbon dioxide, the MCE cell is probably a more advantageous alternative.⁶⁴

One of the primary objectives of present scientific research is the investigation of novel technical methods to reduce CO_2 emission output in the atmosphere. The performance of MCECs for both H_2 production and CO_2 capture has been examined. Due to the combination of the steam reforming reaction, which can be supported inside the cell, and subsequent electrolysis, MCECs can work with CH_4 and H_2O feeding, enabling the syngas or hydrogen production. In this case, MCECs can function as a single, independent system for the generation of hydrogen as well as being retrofitted with reformer units to extend the scope of reforming, allowing for higher CH_4 conversion, production of H_2 , and simultaneous storage of CO_2 . 159

2.1.2. Solid Oxide Electrolysis (SOE)

Donitz and Erdle were the first to publish findings from a solid oxide electrolyser cell (SOECs), used in the HotElly project at Dornier System GmbH in the 1980s. The SOECs incorporated a supported tubular electrolyte. ¹⁶⁰

Recently, SOE cells have proven highly efficient for conversion of water and carbon dioxide to produce carbon fuel and hydrogen, with a high temperature necessary for their conversion and storage. 19 SOEs are divided into two groups in the literature: H+ SOE and O²- SOE. O²- SOE are currently in the demonstration phase, whereas H⁺ SOE is at the lab scale. ¹⁶¹ A dense electrolyte serves as the ionic conductor in SOECs, such as the oxygen ion-conducting SOEC (O-SOEC) and the proton-conducting SOEC (H-SOEC), in which reaction gases such as H₂O or CO₂ are fed into the cathode (or anode) and oxide ions (or protons) are conducted across the dense electrolyte to the cathode (or anode). The evolution of oxygen at the anode enables the cathode to produce fuel gases. 162 This method is very useful to obtain these gases but requires a high production cost (80%) of the energy comes from electricity). 163 Some technical issues are also involved because of the high temperature such as leakage of gas tight components, the requirement of tough materials and its limited application. Moreover, this method has high operation and maintenance costs. Different technological approaches may enhance durability and electro-catalytic performance under low temperature. In renewable energy conversion and storage systems SOE cells have been proven to be a useful and successful technology. 162 The working principle of an SOE cell is shown in Fig 7 162

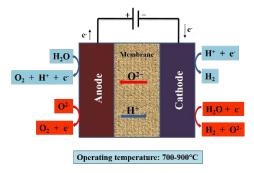


Fig 7: Schematic of SOEC (O/H–SOEC).Red arrows represent the O-SOEC, and blue arrows represent the H-SOEC. Reproduced from ref.¹⁶² with permission from [Springer], copyright [2021].

The endothermic reaction occurs in the SOE cell, while the oxidation reaction occurs at the anode, where oxygen ions move through the electrolyte.

Anode:
$$O^{2-} \rightarrow {}^{1}\!/_{2}O_{2} + 2e^{-}$$
 (11)

Cathode:
$$H_2O + 2e^- \rightarrow O^{2-} + H_2$$
 (12)

Moreover, based on the operating voltage, SOE cells can operate in one of three ways: endothermic, thermoneutral, or exothermic.¹⁶⁴ In endothermic mode, external heat must be applied because the operating voltage is below the thermoneutral voltage; in thermoneutral mode, the required heat is equal to the heat produced by the Joule effect; in exothermic mode, the operating voltage is above the thermoneutral voltage. In order to assure high efficiency and make heat management of SOE cell stacks and systems easier, the most ideal operation mode for an SOE system is the constant thermoneutral voltage (or slightly above in order to account for potential heat losses).¹⁶²

2.2. Low Temperature Water Electrolysis

This type of electrolysis includes following methods:

2.2.1. Alkaline Water Electrolysis (AWE)

Alkaline electrolysis has developed into a mature and well researched technique for hydrogen production up to the megawatt range^{165, 166}since the electrolysis phenomenon was discovered by Troostwijk and Diemann in 1789,¹⁶⁷and now represents the most extensive electrolytic technology at a commercial level worldwide.¹⁶⁸

This type of electrolysis is operated between 30 and 80°C with a concentrated alkaline solution of sodium hydroxide. Moreover, membranes with nickel-catalysed stainless steel and zirconium dioxide are used as a separator. Furthermore, there are various challenges associated with this system due to use of corrosive electrolytes and medium mobility of the hydroxide ions. Due to salt formation of potassium carbonate and sensitivity of electrolyte, decrease ionic conductivity and hydroxyl ions is prominent. Therefore, alkaline water electrolysis produce slower purity hydrogen and oxygen gases since the membrane does not completely stop gases crossing over from one half

of the cell to the other. Generally, the technique consists of two half-cell reactions, with oxygen evolution at the anode and hydrogen evolution at the cathode.¹⁹

Anode:
$$2OH^- \rightarrow {}^{1}\!\!/_{2}O_2 + H_2O + 2e^-$$
 (13)

Cathode:
$$2H_2O + 2e^- \rightarrow 2OH^- + H_2$$
 (14)

In typical alkaline electrolysers, Perovskites are frequently utilised as anodes and Ni-alloys as cathodes. According to reports, efficiency ranges from 59 to 70%. 169

Gas bubbles containing oxygen and hydrogen, respectively, are created on the surfaces of the cathode and anode during the reaction. When the bubbles reach a particular size, they separate off the surface.¹⁷⁰ Several unfavourable events occur in the electrolysis system as a result of the creation of a gas phase. Gas bubbles cover the electrode surface, preventing the flow of electrons from the electrode to the electrolyte. The electrode surface is harmed and the electrolyte's resistance is increased by bubbles.^{170, 171}

The low maximum power density attained with liquid electrolytes is an issue with alkaline electrolysis. This restriction results from the detrimental impact of bubble formation. It is necessary to modify and improve materials and configurations since bubble generation in electrolysis cells is unavoidable. Numerous strategies have been used to counteract these consequences. Although they result in a more complicated system configuration, the use of centrifugal fields, magnetic fields, super gravity fields, ultrasound, and microwave treatments do not considerably increase efficiency. The application of an AEM and a zero gap configuration, respectively, is a very promising technique to enhance the performance of the electrolysis cells. Additionally, operation with an AEM would prevent extra harmful effects of liquid electrolytes. ¹⁷¹ The working principle for an alkaline electrolysis cell is shown in **Fig 8**. ¹⁷⁰

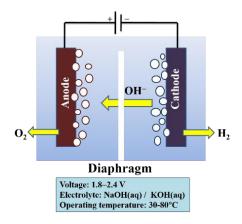


Fig 8: Diagram of an alkaline electrolysis cell. Modified from ref.¹⁷⁰ with permission from [Elsevier], copyright [2010].

In-depth research has been conducted on numerous novel process.es, and some of them have already achieved high efficiency. Anion-conducting membrane alkaline water electrolysers have a number of advantages over alternative technologies. One of the key benefits of alkaline systems over electrolysers utilising proton-conducting electrolytes is the relatively inexpensive cost of the electrode materials because less expensive, non-noble metals are stable in alkaline media.²⁸

However, because of the modest OH⁻ mobility and use of corrosive (KOH) electrolytes, alkaline water electrolysis faces the major difficulty of limited current densities (0.1-0.5 A/cm²).¹⁷²To reduce gas crossing, commercial alkaline water electrolysers frequently employ 2–3 mm thick porous layers.¹⁷³ Device performance is affected by limited ion transport through the layer. Numerous researchers in the past have attempted to create "zero gap" electrolysers, in which a 50–100 mm thick anion exchange membrane is used in place of the 2–3 mm thick porous layer.^{28, 173-177}

Some advancements are still needed to improve this technology to reduce the cross-over of gases and increase current density. Separators and electrode material need to be developed to achieve these challenges, while solar and wind energy sources will be most beneficial for cost reduction. One such avenue recently developed for water splitting is two dimensional metal organic frameworks of nickel nano flakes in alkaline media. Some research organisations/institutes are still actively working in this field to improve efficiency and lower the cost of hydrogen production.

Alkaline water electrolysis mostly takes place by using a Ni based electrolyte and 5M KOH which reduces resistance between porous transport and catalyst layers. Current density should also be increased by ca. 2-3A/cm² using thinner separators with a high surface area of electrode material. For large-scale applications, the alkaline water electrolysis is a good system design. Alkaline water electrolysis now costs between \$500 and \$1,000 per kW, and the system lasts for 90,000 h.^{143, 180}

2.2.2. Proton Exchange Membrane (PEM) Water Electrolysis

PEM electrolysis is the most promising technology when compared to low temperature electrolysis. ¹⁸¹ General Electric and Grubb initially developed PEM electrolysis in the 1950s and 1960sfor space applications to produce oxygen for astronaut life support; submarines were then built using the technology, firstly by Hamilton Sundstrand (now Collins Aerospace). ¹⁸²⁻¹⁸⁵ Since then, a number of businesses have converted the same fundamental technology into goods for hydrogen production at varying scales. The main elements of a PEM electrolyser cell are shown in **Fig 9**. ¹⁸⁵

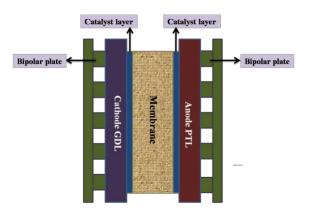


Fig 9: Core components of a PEM electrolyser cell; PTL = porous transport layer; GDL= gas diffusion layer. Modified from ref. 185 with permission from [IOP Publishing], copyright [2021].

In PEM water electrolysis, catalysts based on Pt/Pd are typically used as the cathode for the hydrogen evolution reaction (HER) and catalysts based on RuO₂/IrO₂ are typically used as the anode for the oxygen evolution reaction (OER). An acidic membrane in the form of a solid electrolyte (Nafion, Dupont) and anode and cathode catalysts (mostly Ir and Pt, respectively) make up a PEM electrolyser. The membrane separates the hydrogen and oxygen gases produced by the subsequent reaction while allowing the H⁺ ions to pass from the anode to the cathode. 42

This article is licensed under a Creative Commons Attribution-NonCommercial 3.0 Unported Licence

Open Access Article. Published on 19 October 2023. Downloaded on 10/24/2023 3:00:04 PM.

Anode:
$$H_2O \rightarrow \frac{1}{2}O_2 + 2H^+ + 2e^-$$
 (15)

Cathode:
$$2H^+ + 2e^- \rightarrow H_2$$
 (16)

At the anode, hydrogen molecules break apart, which ionises the atoms and sends their electrons into an external circuit; through an ion-exchange membrane protons congregate at the cathode. Oxygen, protons from the ion-exchange membrane, and electrons all then come together to afford water or steam. We can get an energy conversion efficiency of 60% or more with this method. 191, 192 The working principle of PEM electrolysis cell is shown in **Fig 10**.

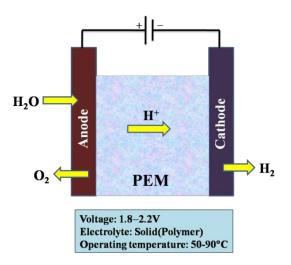


Fig 10: Illustration of a PEM electrolysis cell.

Membrane electrode assemblies (MEAs), current collectors (gas diffusion layers), and separator plates make up the majority of the parts of a PEM water electrolysis cell. **Fig 11** depicted a typical overall view of a PEM water electrolysis cell assembly. However, MEA, which divides the cell into two half cells (anode and cathode), is at the centre of the electrolysis cell.¹⁸¹

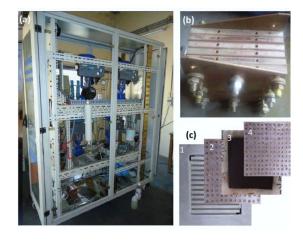


Fig 11:a) Overview of typical PEM water electrolyser,**b)** PEM cell stack and,**c)** cell components; 1-bipolar plate, 2-anode current collector, 3-MEA, 4-cathode current collector. 181

These proton exchange membranes offer a number of benefits, including low gas permeability, robust proton conductivity (0.1± 0.02 S cm⁻¹), reduced thickness (20–300 μm), and high-pressure operations. PEM water electrolysis is one of the preferable technologies for converting renewable energy to highly pure hydrogen from a sustainability and environmental perspective. Other excellent attributes offered by the PEM water electrolysis method are a small carbon footprint, high current densities (over 2 A cm⁻²), lower operating temperatures (20–80°C), ultrapure hydrogen production, and the production of oxygen as the by-product.^{20, 27, 193-195}The purity of the gases produced is higher than that of alkaline electrolysis.⁴² As a result, when compared to alkaline electrolysis, PEM electrolysis can achieve great efficiencies(50–75%) with a quick response.¹⁷

The PEM electrolyser is expected to cost between \$1000 and \$1400 per kW, with clear paths to be reduced to \$400. The \$1/kg H₂ target set forward in the US Department of Energy's Hydrogen Energy Earth Shot campaign must be reached in order to reach its ultimate goal of \$150/kW. Due to the acidic nature of the electrolyte with strong proton conductivity and the structures that reduce ohmic losses, the water electrolysis kinetics in PEM cells are faster than in alkaline electrolysis. The capability of applying a high pressure on the cathode side while operating the side of the anode at atmospheric pressure is a beneficial aspect of PEM electrolysis. ¹⁸⁵

However, cost and durability continue to be obstacles preventing PEM electrolysers from being widely used. To research the deterioration of PEM electrolysers and further increase their durability, collaborative accelerated stress tests across many laboratories are extremely

desirable.¹⁸⁵ The usage of expensive polymeric membranes and the need for noble metals due to the electrolyser's acidic liquid are current drawbacks. One of the main difficulties is reducing the amount of noble metals used in PEM electrolysers.¹⁸¹ The adoption of platinum group metals as noble metal catalysts, Nafion-based membranes, and Ti-based stack materials are causes PEM water electrolysis expenditure issues.⁴²

2.2.3. Anion Exchange Membrane (AEM) Water Electrolysis

AEM electrolysis cell consist of electrode made of transition metals catalyst and hydrocarbon anion exchange membrane. Purified water or a low concentration alkaline solution can be used as the electrolyte in the AEM in place of a strong KOH solution (**Fig 12**). Anion exchange membrane water electrolysis combines the advantage of alkaline electrolysis and proton exchange electrolysis. ^{177, 196, 197}AEM electrolysis technology, like alkaline and PEM electrolysis, use low-cost catalysts and a solid polymer electrolyte. ¹⁹⁸ It works in an alkaline environment, which allows for the use of low-cost electrocatalysts and a zero-gap architecture. ¹⁹⁹ This method of electrolysis employs a polymeric membrane containing quaternary ammonium salts. It is relatively cheap and has little interaction with surroundings CO₂. ^{200, 201}

AEM electrolysis is projected to outperform conventional electrolysis technologies in terms of performance and total cost.²⁰² Previous research with AEM electrolysis has yielded promising outcomes. One study found that a membrane electrode assembly (MEA) combination of polybenzimidazole (PBI) AEM and specific catalysts (Ni-Fe-Ox for oxygen evolution and Ni-Fe-Co for hydrogen evolution) performed best under specific conditions, with an AEM electrolysis efficiency of 74% at 1000 mA cm², 1.9 V, and 60 °C.²⁰³

Despite its satisfactory performance, the AEM electrolyser's performance is lower than that of traditional PEM electrolysers. ^{198, 199}In AEM electrolysers, the voltage drives the electrolysis reaction, whilst the current reflects the rate of hydrogen generation. When a voltage is supplied between the anode and cathode, electrons travel via an external circuit and are balanced by the movement of hydroxideions through the AEM. ²⁰⁴The hydroxide ions strive to cross the AEM when more voltage is applied, while the electrons will travel via the external circuit. However, at lower voltages, electrons and OH-cannot transfer due to internal barriers. ²⁰⁵

A drop in voltage causes a decrease in hydrogen production, termed charge transfer resistance or activation over potential. And if the applied voltage is low, the flow of electrons is restricted by internal components such as the catalyst layer, AEM, and gas diffusion electrode (GDL). The ohmic resistance (R_{ohm}) is the name given to this constraint. ²⁰⁶However, the performance of an AEM electrolyser is determined by three variables: kinetic resistance, ohmic resistance, and mass transfer resistance. ^{207, 208}

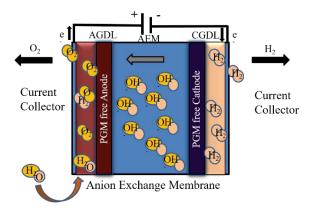


Fig 12: Working principle of an AEM electrolysis cell.

2.3. Solar-powered Water Electrolysis

Renewable energy electrolysis would produce an exceptionally clean hydrogen cycle (**Fig 13**). Solar (and wind) generated hydrogen could meet the world's anticipated energy needs, however, delivering it may cost more than making hydrogen from natural gas.²⁰⁹

This article is licensed under a Creative Commons Attribution-NonCommercial 3.0 Unported Licence.

Open Access Article. Published on 19 October 2023. Downloaded on 10/24/2023 3:00:04 PM.

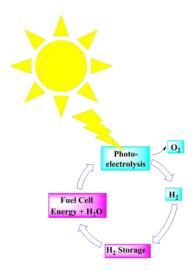


Fig 13: A renewable hydrogen cycle. Modified from ref.²⁰⁹ with permission from [Elsevier], copyright [2002].

Solar-powered water-splitting for hydrogen production is a clean and viable energy solution; two promising technologies for this are photovoltaic-electrocatalysis(PV-EC) and photoelectrocatalysis(PEC). A photoelectrode harvests light and electrolyses water in the PEC process. PV-EC incorporates separate modules for solar-powered electricity generation and water-splitting (**Fig 14**), distinguishing PV-EC from a standard PEC configuration.¹²¹

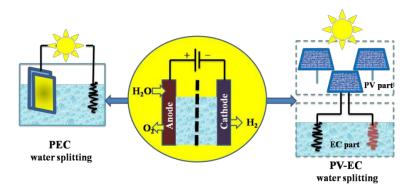


Fig 14: Two pathways for solar hydrogen production by PEC and PV-EC water splitting. Modified from ref.¹²¹ with permission from [Springer], copyright [2021].

2.3.1. Photoelectrochemical (PEC) Cells

The process of PEC water splitting produces hydrogen fuel from sunlight. Sunlight strikes the photoactive electrode, producing electron-hole pairs, which is the first of four steps. Water is oxidised by the photo-generated holes, and electrons are transferred to the photocathode. Proton (H⁺) undergoes reduction at the photocathode, creating hydrogen gas. It is possible to separate carriers effectively by employing an external power source. For electron generation, the photoactive material needs to have the appropriate band gap. The process is also impacted by semiconductor band locations. Due to its clean operation and direct conversion of sunlight, PEC-based hydrogen production is gaining popularity as a sustainable method of producing hydrogen.²¹⁰

It is generally agreed that Brattain, Garret,²¹¹ and Gerischer's²¹² research established the groundwork for contemporary photo-electrochemistry. Numerous articles on photo electrochemical cells emerged in the wake of the 1973 oil crisis, which prompted an increase of new study into renewable energy sources.²¹³ The focus was on two types of cells: regenerative cells and photosynthetic cells. Light is converted to electric power by regenerative cells without generating any net chemical change. Photon-generated electron-hole pairs are separated, with negative charge carriers passing through the semiconductor to the current collector and external circuit and positive holes being collected by a redox relaying molecule. Water is oxidised to oxygen at the semiconductor photoanode and reduced to hydrogen at the cathode in photosynthetic cells, which work similarly but include two redox systems as shown in **Fig 15a**.²¹²

After the 1972 Nature paper by Fujishima and Honda showing photo-driven water oxidation on TiO₂ with a small bias, the idea of a single material PEC-cell that could drive both photo-oxidation and photo-reduction of water without an external bias was developed.²¹⁴ A single substance immersed in water to make hydrogen and oxygen, making this idea interesting. However, there are several prerequisites, such as the material requiring a large band gap to generate energy but not one that is too large to absorb sunlight. Band edges must align with exact energy levels to enable water oxidation and reduction processes (**Fig 15b**). The material should be able to separate and transport light-generated charge carriers without recombination. The interface of the material

should also be catalytically active for water oxidation and reduction, as well as stable in water and light. The material should also be non-toxic and affordable.

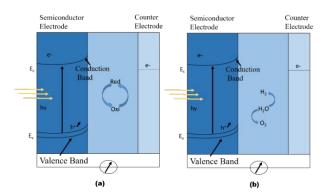


Fig 15: Working principle of photo-electrochemicalcells. Reproduced form ref.²¹² with permission from [Nature Publishing Group UK London], copyright [2001].

Substantial effort has been put into discovering a suitable material for efficient PEC water splitting. 215-217 Hundreds of compounds were investigated using combinatorial methods. 218-220 All requisitions, however, have not been met by any material. Using a plethora of materials to create a PEC device is more efficient since the stresses on each material are reduced. Instead of relying on each element to be efficient at everything, synergy of the materials can accomplish what is required. Putting distinct functionalities into a variety of materials has been beneficial in the development of useful technologies.

Different approaches to monolithic device design incorporating many materials are studied in the research literature. One way to do this is to make a group of monoliths that are suspended as nanoparticles.^{217, 221, 222} This method is appealing because it is simple, there is no need for wires, wiring, or separating the cells. It can also be made with sol-gel synthesis methods, which can be used on the large scale and possibly be less expensive.²²³ Small particles are used in diffusion to split and move charges. Co-catalysts increase the activity of surface catalysts; two co-catalysts can be used, however, this increases difficulty. This design makes oxygen and hydrogen at the same time, which raises worries about back reactions and so induces the additional requirement of gas separation in another second step. Because the particles are so small, it's hard to tell which ones do what. This limits which materials that can be used, but not as much as with single-material

monoliths. **Fig 16c** shows a monolithic cell with multiple layers. Pure PEC cells, underground PV junctions, and PV-electrolysis can employ this type of design. This design is larger than the nanoparticles in suspension approach, making material selection and combination easier. This design has yielded multiple functioning devices, including the 2.5% efficient "artificial leaf" and a 10%efficient CIGS (thin-film solar cell) device.²²⁴

Separating the cathode and anode spatially changes the perspective from a multi-layered PEC cell. Instead of passing through a back contact to a second electrode, the majority carriers can be wired to the counter electrode; the only difference is charge distance. This method uses a macroscopic wire and a resistive element. The main benefit is greater freedom in geometrical arrangements, synthesis techniques, and material choice. This topological transition lets electrodes be developed, manufactured, and studied separately in an attempt to boost device performance.

There are numerous designs of this concept. One involves a photoactive electrode and a counter electrode performing a sole catalytic function which constitutes the simplest configuration (**Fig 16a**). Either a p-type semiconductor photocathode or an n-type semiconductor photoanode, as in **Fig 16a**, can serve as the photoactive electrode. The devices produced by Khaselev*et al.*^{225, 226} and Recee*et al.*²²⁷ show that the single photoactive electrode can be configured as a tandem cell. **Fig 16b** illustrates a more sophisticated technique that employs two photoactive electrodes to create a spatially separated tandem cell. For instance, Abdi *et al.*²²⁸ constructed a 4.9% efficient device using BiVO₄ and a tandem junction a-Si solar cell, while Brillet*et al.*²²⁶ presented a 3.1% efficient device using WO₃ and a dye-sensitizsed solar cell as examples.

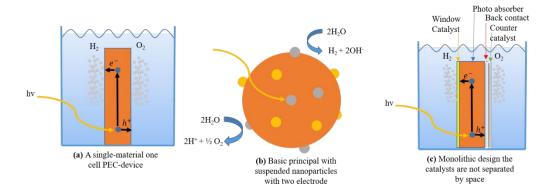


Fig 16: a) A single-material one cell PEC-device. **b)** Basic principal with suspended nanoparticles with two electrodes. **c)** Monolithic design where the catalysts are not separated in space.

Researchers may improve each step and look into the fundamental functioning of the system by looking at the two half-reactions separately. Through photocurrents, the macroscopic charge transport makes it simple to gauge efficiency. Once the materials for both half-reactions have been determined as being effective, they can be joined to form a device for the full reaction. In the literature, a number of substances have been investigated for their potential to act as catalysts in these half-reactions.²¹⁵⁻²¹⁷

2.3.2. Photovoltaic Cell (PVC)

In a PEC, a configuration called PV-electrolysis involves spatially isolating the catalysts. The monolithic design in **Fig 17a** serves as the starting point for the process. Separating one of the catalysts into a different electrode is one step toward PV-electrolysis, as shown in **Fig 17b**. A three-electrode setup, as shown in **Fig 17c**, can be created by separating the second catalyst from the photo-absorber to further improve the configuration.

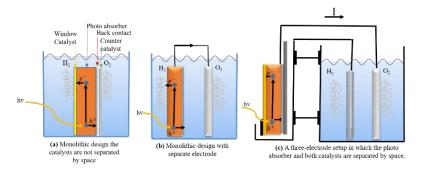


Fig 17: a) Monolithic design where the catalysts are not separated by space. b) Monolithic design with separated electrode. c) A three-electrode setup in which the photo absorber and both catalysts are separated by space.

PV-electrolysis is technologically mature because the PV (photovoltaic) part and the catalysts can be developed, improved, and tested separately. They can be connected directly, as shown in **Fig** 18a, or through the power grid, as shown in **Fig** 18b.

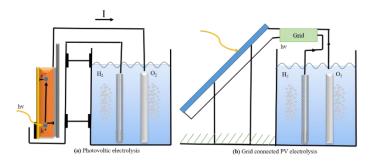


Fig 18: a) Photovoltic electrolysis. b) Grid connected PV electrolysis.

The transmission efficiency of electricity across power lines is approximately 93%, with loss of 7%.²²⁹Hydrogen electrolysers often make use of expensive resources and run at high levels to maximise efficiency and minimise costs. Unfortunately, this causes a loss of efficiency. However, other types of electrolysers can be even more efficient than alkaline ones. The biggest problem with these systems is the price, not how well they work. Creating hydrogen from natural gas is less expensive than using solar cells, but that could change in the future. Then, attention will turn to improving the process's catalysts.

Directly connecting the solar cell to the electrolysers, rather than going through the grid, avoids the need for inverters and decreases grid losses. Since this lowers solar cell and electrolysers prices,

it can make the system more competitive in the market. But there is a disadvantage since the electrolyser's power supply is less stable, its efficiency may suffer as a result. The benefit of disconnecting from the grid and inverters can be nullified if this happens.²³⁰

2.4. Grid connected Water electrolysis

Grid electrolysis involves connecting the electrolyser to an existing electrical network. During the transition to a prosperous hydrogen economy, this approach appears to be the shortest and least expensive. However, using this technique, hydrogen production is not practicable in isolated or rural areas lacking access to dependable electricity. Additionally, even though electrolysis does not directly release any harmful gases to the environment, it indirectly harms the environment by increasing the combustion of fossil fuels to produce electricity. Numerous research effort has focused on various elements of grid electrolysis, such as energy storage and grid balancing.²³¹ Currently, it is believed that the most practical method for producing hydrogen during the switch to vehicles powered by hydrogen is grid electrolysis (e.g., fuel cell vehicles).^{232, 233}There is more information available on grid electrolysis and its potential for producing sustainable hydrogen elsewhere.²³⁴⁻²³⁶

Various variables, such as the capital expenditures of controlling peak demands, the investments required for grid reliability, and the integration of renewable energy sources, might be linked to the rising interest in energy storage for the grid. There is acknowledgment that battery systems can offer a variety of high-value options, assuming that reduced costs can be reached, even if pumped hydropower is currently the dominant form of energy storage. The battery systems including redox-flow batteries, which are inexpensive, lithium-ion batteries, developed for commercial gadgets and electric vehicles, and sodium-sulfur batteries, which are commercially accessible for grid applications. ¹⁰²

Several electrolyser stacks, compressors, and gaseous hydrogen storage units make up a large-scale water electrolysis hydrogen production system (Fig 19). We take into account hydrogen production from electrical grids with strong renewable energy penetration and usage in a variety of applications across various industries. This system layout was primarily chosen based on the input needs of feedstock hydrogen in the subsequent chemical processes related to the production of hydrocarbon fuels, industrial use, or fuel supplied in the production of electricity. A developed

hydrogen value chain is necessary for centralised electrolytic hydrogen production, which is also applicable to the transportation industry. More significantly, the integration of renewable energy sources into the power grid through the use of water electrolysis and the production of hydrocarbon fuel (synfuel) creates a process that can decarbonize the energy supply chain. By turning electricity into hydrogen, the inclusion of large-scale water electrolysis into the power grid might reduce the volatility of renewable energy sources. The installed capacity of the water electrolysis facility is anticipated to vary from several MW to 100 MW, or possibly GW, for the case of synfuel production on a massive scale.²³³

The key distinction from typical chemical processes, such as Steam Methane Reforming (SMR), is the use of water and electricity rather than coal or natural gas (NG) in an electrolyser that is connected to the grid to generate hydrogen. Additional sources of electricity include 26 MW and 54 MW solar and wind farms, respectively. The following possibilities are listed:

- ✓ An electrolyser that is grid-connected receives power from the exterior public electrical grid;
- ✓ Wind turbine (WT)/Grid-connected Electrolyser: The grid and wind turbine both provide energy to the electrolyser. A portion of the electricity generated by the WT is marketed to the electricity market because the wind turbine is greater than the electrolyser capacity;
- ✓ Photovoltaic(PV)/ Wind turbine (WT)/Grid-connected Electrolyser: The grid-connected electrolyser is powered by PV and WT, and some of the electricity is sold to the electricity market;
- ✓ PV/Grid-connected Electrolyser: The grid and PV work together to supply energy to the electrolyser. A portion of the electricity generated by PV is distributed to the electrical market since the PV capacity is greater than the electrolyser capacity.²³⁷

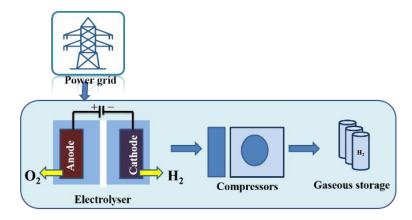


Fig 19: The water electrolysis technique for producing hydrogen (Grid electrolysis process). Reproduced from ref.²³³ with permission from [Elsevier], copyright [2019].

To create the techno-economic model for a grid-connected large-scale hydrogen production plant, three possibilities are taken into account (as illustrated in **Fig 20**). This model also takes different power price structures, hydrogen generation and storage systems, and component sizes into account.

- ✓ In Scenario 1, when electricity costs are defined as fixed charge rates, the impact on a levelized cost of hydrogen is examined. Since the operation schedule reflects the output demand, hydrogen storage is not taken into consideration. For medium-scale implementation, the average outputs are set at 4000 kgH₂/day, and for large-scale deployment, at 40,000 kgH₂/day.
- ✓ In Scenario 2, a metal tank at 200 bar is used to examine the impact on a levelized cost of hydrogen at wholesale energy markets with a 1-day storage capacity. The storage capacity (40,000 kgH₂) is viewed as being sufficient for one day. From 0.4 to 1.0 capacity factors are taken into account. The adaptability of areas where large-scale geological hydrogen storage is not practical is taken advantage of by this system arrangement.
- ✓ Scenario 3 investigates the impact of massive underground hydrogen storage on a levelized cost of hydrogen at wholesale energy markets. The production facilities anticipate that taking into account a 7-day storage capacity will allow them to further benefit from cost savings during non-peak times. The capacity factor is rated from 0.4 to 1.0, just like in scenario 2.²³³

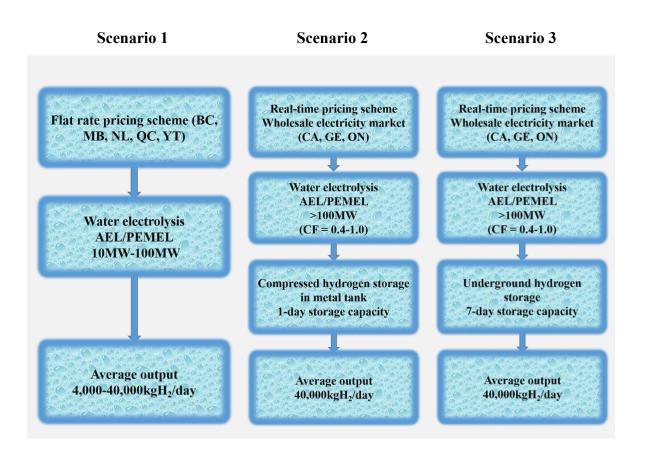


Fig 20: Deployment scenarios for water electrolysis. (BC = British Columbia; MB = Manitoba; NL = Newfoundland and Labrador; ON = Ontario; QC = Quebec; YT = Yukon; CA = California; GE = Germany). Modified from ref.²³³ with permission from [Elsevier], copyright [2019].

2.5. Wind-powered Water Electrolysis

In wind electrolysis, the electrolyser is connected to the power generated by wind turbines. It is possible to create cleaner hydrogen using wind electrolysis, which also holds the potential to make greater use of the renewable energy sources that are already present in the area²³⁸ and to increase the proportion of renewable energy in the electric grid while lowering greenhouse gas emissions.²³⁹ However, hydrogen generation from wind electrolysis needs to be competitively priced to allow for a higher uptake of renewable energy sources e.g. to compete with gasoline or other vehicle fuels as a vehicle fuel or being cost-competitive with other grid electricity technologies as a grid

energy storage technology.^{240, 241}At some wind production sites, hydrogen production could be achieved at\$4/kg or less.²³⁶ The capacity factor, which must be 44% or more together with reasonably high wind speeds, is a major problem.²⁴² Nevertheless, in addition to low production costs, delivery and storage costs will also affect the final pricing of hydrogen. For this reason, it is necessary to investigate a wider variety of wind sites, where geographical factors such as distance from the end usage should also be taken into account.⁵²

The concept underlying the coupling system between non-grid connected wind power and water electrolysis holds that when "three fields"—temperature field, electric field, and flow field—are balanced, the large-scale fluctuations in wind power current density have little effect on water electrolysis efficiency in the electrolyzer. Improvements should be made to cooling systems, power supplies, and water-electrolytic technologies to address the effects of wind power variation on production. The electrolyzer utilizes an intelligent power controller to accomplish "seamless connection without disturbing each other" and to create "wind power-based, grid power-supplemented" systems. The intelligent power controller has two supply models, referred to as wind/grid complementary power supply and wind power independent supply. Wind power will be completely used, regardless of wind speed. There are three scenarios:

- ✓ when wind power is greater than the rated power of the electrolyzer, no grid power is used:
- ✓ when wind power is lower than the rated power of the electrolyzer, grid power is complimentary;
- ✓ and when there is no wind, grid power supplies all of the power. Gird electricity is used by the water circulation pump and other auxiliary devices.

In accordance with the wind conditions, the flow of cooling water is also adjusted. In order to improve the water electrolyzer, "three-field" balancing was thus attained. **Fig 21** depicts the circuit diagram of a water electrolytic hydrogen generation system that uses wind energy without a grid connection.²⁴³

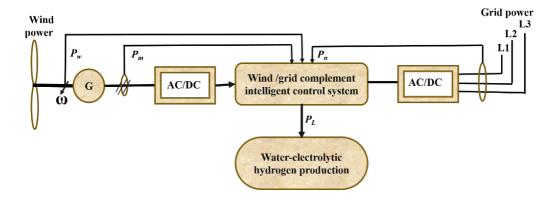


Fig 21: Circuit diagram of non-grid-connected wind power/water-electrolytic hydrogen production system. Modified from ref.²⁴³ with permission from [Elsevier], copyright [2012].

Electricity generation from wind energy illustrated minimum negative impacts on the environment compared to the other energy resources.²⁴⁴ In 2012, about 282,275 MW electricity was generated by wind energy which was around 2% of total world electricity demand. USA, China, Germany, Spain, and India generate more than 73% of annual worldwide wind electricity.²⁴⁵ In order to utilise the maximum capacity of wind power, complex wind power plants should be managed wisely. For instance in some wind power plants around the world, the transportation capacity of the electricity grid should be upgraded and additional power capacity should be installed to prepare a backup for the installed wind power system.

Wind energy can vary due to meteorological changes, which increases the demand for balancing power in load frequency regulation. Such issues might be resolved using a water electrolysis-based wind to hydrogen (WTH) technique. In times of low wind potential or after grid congestion has subsided, the excess electricity is stored as hydrogen and converted back into electricity.²⁴⁶ For both grid-connected systems and isolated grid systems, electrolytic hydrogen's potential as a storage medium for wind energy in network balancing has been researched.^{247, 248}Hydrogen serves as a buffer for wind power facilities to control changes in wind power due to the synergy between the sectors of hydrogen energy and wind power.²⁴⁹ Additionally, the WTH system has a great deal of potential for use in light-duty cars as a clean fuel to reduce rising GHG rates.²⁵⁰ An integrated system for producing electricity from wind energy and using hydrogen is shown in **Fig 22**.²⁵¹

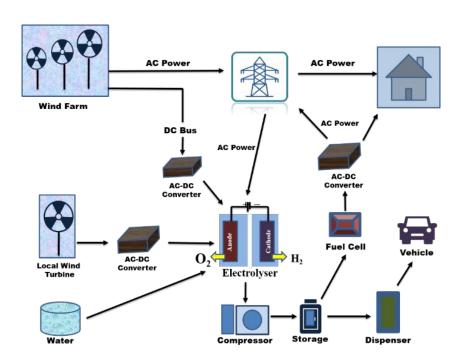


Fig 22: Integrated wind energy system for producing electricity and hydrogen. Modified from ref.³⁴ with permission from [Elsevier], copyright [2016].

By producing hydrogen from natural gas and gasoline as non-renewable fuels, Granovskii*et al.* completed a life cycle assessment (LCA) of hydrogen and power generation from wind and solar technologies as renewable resources. It was stated that the cost of hydrogen produced through the reforming of renewable sources is higher.²⁵² Additionally, it was noted that WTH for hydrogen vehicles fuel cells instead of gasoline can result in a cost-effective reduction of GHG emissions when the efficiency of an hydrogen vehicle is two times higher than an internal combustion vehicle.²⁵³ Due to the high cost of newly installed equipment and energy loss from inefficient energy conversion processes, hydrogen produced from wind energy is expensive.²⁵⁴

According to Harrison *et al.*, the National Renewable Energy Laboratory (NREL) in the US oversaw the testing of a WTH pilot scale that connects 100K wind turbines with polymer electrolyte membrane (PEM) and an air energy storage system (AES) that produces 20 kg of hydrogen per day. The price of the hydrogen produced by this technique is approximately \$5.50/kg, however this price can be reduced by installing cutting-edge wind turbines, and the cost objective for 2017 is \$2/kg. It is significant that when the price of the WTH system falls to \$0.015/kWh, hydrogen production using the technology might be competitive with hydrogen generation using gasoline.²⁵⁵

2.6. Nuclear Energy-powered Water Electrolysis

It is appealing to use nuclear energy as the main source of energy for hydrogen production because it is adaptable to large-scale hydrogen production and its greenhouse gas emissions are significantly lower than those associated with conventional fossil fuel combustion. Through numerous studies that were published in the open literature in recent years, advancements in nuclear-based hydrogen production have become apparent. Connecting an electrolyzer to a nuclear power station is the easiest way to produce hydrogen from nuclear energy (Fig 23). Such a system has the advantage of being able to run at design load without directly interfering with the grid, which can experience grid overload at times.

The fact that there is no need to modify the reactor is another significant benefit of nuclear/water electrolysis. Such systems were used on nuclear submarines to produce hydrogen and oxygen, which are both necessary for life. The system can be modified to use existing nuclear power reactors to produce off-peak electricity. Nuclear power facilities can operate at constant load with the maximum efficiency and lowest cost of electricity generation by producing hydrogen during off-peak hours. Additionally, potential grid congestion is avoided, enhancing the electrical grid's effectiveness and reliability. Remember that even while tested approaches only achieve less than 55% efficiency, the maximum predicted efficiency of the water electrolysis process is 80%. The presented thermal-to-hydrogen efficiency when coupled to modern light water reactors or advanced light water reactors (ALWR) is 27%; however, when coupled to modular helium reactors (MHR) or advanced gas reactors (AGR), the expected efficiency is 35%.

Nuclear reactors have typically been used to generate electricity using steam power plants. According to studies, if a sustainable fuel like hydrogen is created in addition to electricity, there will be more advantages. When using nuclear energy, higher temperatures and pressures are required for the reactor coolant since the efficiency of power generation typically increases as the working medium's temperature rises. However, the allowed temperatures in nuclear reactors and the corresponding temperatures and pressures of the coolants are what primarily restrict advancements in the power generation efficiency of nuclear power plants. The rates of material corrosion and safety restrictions on nuclear reactors set a limit on coolant parameters.

Numerous studies focus on the advancement of nuclear reactors, which must match certain criteria like providing inexpensive energy and high temperature heat in order to effectively couple it with a hydrogen manufacturing facility. The most promising hydrogen generation systems, in terms of the process heat temperature level they offer, are gas-cooled reactors, molten salt-cooled reactors, and heavy metal-cooled reactors. The various nuclear reactor technologies along with nuclear reactor-adaptable thermally-driven hydrogen production processes will complement rather than compete in the development of nuclear-based hydrogen generation in the future.¹⁷

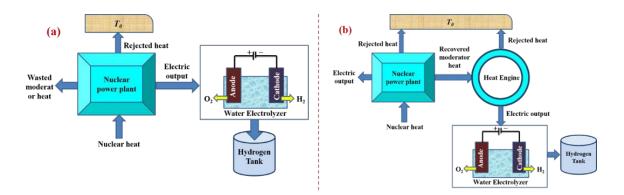


Fig 23: Approaches for integrating nuclear reactors and water electrolysis for **(a)** dedicated hydrogen production systems or **(b)** cogeneration systems of electricity and hydrogen. Modified from ref.¹⁷ with permission from [Elsevier], copyright [2012].

3. Electrolysis Using Organic Fuels

Despite the fact that water or steam electrolysis is well recognised, its extensive application is constrained by high operational costs associated with energy use. Utilising an alternative anode reaction for O_2 evolution with a lower equilibrium potential can reduce the amount of electrical power needed for electrolysis. Several reactions can be employed to do this, but one that has the potential to be appealing is the use of an organic chemical fuel. Methane gas is one such method, which is used as an anode depolariser.²⁵⁶

Anode:
$$CH_4 + 2H_2O \rightarrow CO_2 + 8H^+ + 8e^-$$
 (17)

Cathode:
$$8H^+ + 8e^- \rightarrow 4H_2$$
 (18)

The traditional method of electrolysis is water electrolysis, however, because it uses so much energy, interest in producing hydrogen by methanol electrolysis has grown due to several benefits over traditional water electrolysis.²⁵⁶⁻²⁵⁸

By effectively substituting one unit of electricity with one equivalent energy unit of natural gas at a cheaper cost, this is analogous to electrochemical steam reforming. High system efficiency in terms of primary energy is made possible with the use of natural gas in the electrolyser; voltage reductions of up to 1.0 V in comparison to conventional electrolysers are feasible, and as a result, the electrolyser's electricity consumption can be as low as one-third of that of conventional electrolysers. ²⁵⁶⁻²⁶¹ However, since it utilises natural gas, this method is not sustainable. Alcohol, which may be produced via fermentation technology, can be the basis of an alternate system. One such methanol-powered cell circulates an aqueous solution past the anode, where methanol and water combine to produce carbon dioxide, much like that in a direct methanol fuel cell:²⁵⁶

Anode:
$$CH_3OH + H_2O \rightarrow CO_2 + 6H^+ + 6e^-$$
 (19)

Cathode:
$$6H^+ + 6e^- \rightarrow 3H_2$$
 (20)

The electrolysis was carried out using a DC power supply to deliver a constant current to the electrolytic cell. A platinum resistance thermometer was positioned close to the anode surface to gauge the electrolytic cell's temperature. Water and the methanol-water solution were then given to the electrolytic cell's anode. A non-pulsation quantitative pump was used to regulate the flow rates and the electrolytic cell's membrane electrolyte was a Nafion–117 membrane. Both the anode and the cathode catalyst were made of platinum.²⁵⁶ Additionally, methanol cross-over from an anode to a cathode in Nafion membrane methanol electrolysers increases fuel consumption and results in contaminants in the hydrogen produced; as a result, membranes have been further developed to solve this issue.²⁶¹⁻²⁶⁴ Fig 24 indicates the electrolysis setup for organic fuel methanol.

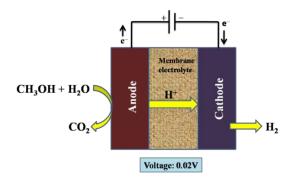


Fig 24: Electrolysis using organic fuel methanol.

A research study explained the exceptional performance of a CoS₂nanoarray electrode on a titanium mesh substrate (CoS₂/TiM) as a highly efficient and durable catalyst for the oxidation of hydrazine in a 1.0 M KOH electrolyte containing 100 mM hydrazine. Achieving a current density of 100 mA cm⁻² requires only a low potential of 125 mV. The impressive hydrogen-evolving activity exhibited by CoS₂/TiM positions it as a versatile bifunctional catalyst for energy-efficient hydrogen production through electrolysis, where it replaces the conventional water oxidation with hydrazine oxidation. In an electrolyzer operating at 100 mA cm⁻², CoS₂/TiM demonstrates remarkable performance, with a minimal cell voltage requirement of just 0.81 V in a two-electrode setup. Furthermore, it exhibits outstanding long-term electrochemical stability and achieves nearly 100% Faradic efficiency for the evolution of hydrogen gas.²⁶⁵

An effective strategy to substantially reduce the voltage required for water electrolysis is to substitute the anodic OER with the hydrazine oxidation reaction (HzOR) due to its lower thermodynamic oxidation potential. In a study, researcher designed a novel copper–nickel nitride (Cu₁Ni₂-N) catalyst with a well-defined Cu₄N/Ni₃N interface on a carbon fiber cloth substrate. This three-dimensional (3D) electrode demonstrates exceptional performance in HER, requiring only a minimal over-potential of 71.4 mV at a current density of 10 mA cm⁻² in a 1.0 M KOH solution. Simultaneously, it exhibits an impressively low potential of 0.5 mV at 10 mA cm⁻² for HzOR when used in a 1.0 M KOH/0.5 M hydrazine electrolyte. Furthermore, when this synthesized Cu₁Ni₂-N electrode is employed as both the cathode and anode in an electrolytic cell, it achieves a cell voltage of 0.24 V at 10 mA cm⁻² and maintains excellent stability over a 75-hour duration. This research represented a significant step forward in the development of copper–nickel-based nitrides as bifunctional electrocatalysts, leveraging hydrazine assistance to enable energy-efficient hydrogen production through electrolysis(Fig 25).²⁶⁶

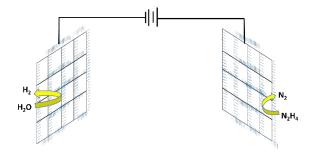


Fig 25: Electrolysis using organic fuel hydrazine. Modified from ref.²⁶⁶ with permission from [Wiley Online Library], copyright [2019].

A research study investigated an energy-efficient alkaline hydrogen production system by substituting the oxygen evolution reaction (OER) with the more oxidizable urea oxidation reaction (UOR). In this context, a bimetal heterostructure, CoMn/CoMn₂O₄, was engineered to serve as a bifunctional catalyst within an alkaline environment, facilitating both urea oxidation and the hydrogen evolution reaction (HER). The CoMn/CoMn₂O₄heterostructure, characterized by a Schottky heterojunction structure, enables spontaneous charge transfer at the interface. This feature enhances the adsorption of reactant molecules and the breaking of chemical bonds, thereby initiating the decomposition of both water and urea. Consequently, the heterostructured electrode demonstrated remarkably low potentials of -0.069 V and 1.32 V (versus the reversible hydrogen electrode) to attain current densities of 10 mA cm⁻² for HER and UOR, respectively, in an alkaline solution. Furthermore, the complete urea electrolysis driven by CoMn/CoMn₂O₄ achieves a current density of 10 mA cm⁻² at a relatively modest potential of 1.51 V and maintains stable performance for over 15 hours. This innovative approach involving Mott-Schottky hybrids in electrocatalysts represented a promising avenue for sustainable energy conversion, merging hydrogen production with sewage treatment for environmentally responsible applications(Fig 26).²⁶⁷

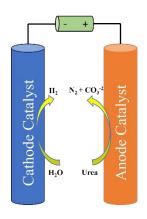


Fig 26: Electrolysis using organic compound urea.

In another study researchers substituted the OER with the thermodynamically preferred 5-hydroxymethylfurfural (HMF) that give 2,5 furan dicarboxylic acid (FDCA) on oxidation. They created three-dimensional (3D) hybrid electrocatalytic electrodes by layering nanosized graphene oxide as a building block. These electrodes were capable of aiding both HMF conversion and the hydrogen evolution process (HER) at the same time. The nanoarchitecture of the electrode, comprising the thickness and position of gold (Au) and palladium (Pd) nanoparticles (NPs), was found to have a substantial influence on electrocatalytic performance. Even when the same constituent NPs were used, the electrodes demonstrated highly adjustable performance via reaction kinetics and diffusion-controlled mechanisms. Furthermore, in a full-cell setting, a bifunctionaltwo-electrode electrolyser optimised for HMF oxidation and HER had the highest overall electrocatalytic activity.

Anode: HMF + $6OH^- \rightarrow FDCA + 4H_2O + 6e^-$

Cathode: $6H_2O + 6e^- \rightarrow 3H_2 + 6OH^-$

Overall HMF+2H₂O \rightarrow FDCA+ 3H₂

In a recent study, researchers introduced a novel integrated electrode composed of CoNiPnanosheets with a dual functionality. The CoNiP-NIE serves to enhance the HER while also replacing the OER with the oxidation reaction of 5-hydroxymethylfurfural to produce the valuable compound 2,5-furandicarboxylic acid (FDCA). Newly designed electrode achieves a high Faradaic efficiency exceeding 82% for HMFOR over a wide potential range, from 1.40 V to 1.70 V vs. RHE (reversible hydrogen electrode, which surpasses the performance of previously reported

electrocatalysts. Furthermore, the low overpotential required for HER underscores its effectiveness in hydrogen (H₂) generation. Leveraging the bifunctional properties of CoNiP, researchers constructed an electrochemical device that combines hydrogen evolution with biomass oxidation. This device exhibits a lower voltage requirement (1.46 V) for anode oxidation compared to traditional water splitting (1.76 V) and achieves a higher H₂ evolution rate (41.2 L h⁻¹ 1 m⁻²) under the given conditions (Fig 27).

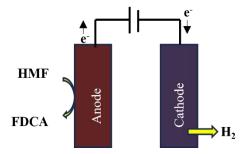


Fig 27: Schematic illustration of HMFOR and HER. Modified from ref.²⁶⁸ with permission from [Elsevier], copyright [2022].

4. Hydrogen as a By-product from Electrolysis

Numerous electrolyses are based on anodic oxidation, which is accompanied at the cathode by hydrogen evolution. The electrolysis of the halides results in a variety of compounds, which is notable. The chemistry and electrochemistry of the halides (Br, Cl, and I) involve reactions that are quite similar, although the values of the kinetic and thermodynamic parameters vary. Chlorine electrochemistry is a significant field of industry. An important illustration is the electrolysis of sodium chloride to produce chlorine and sodium hydroxide (the chlor-alkali process). The desired reaction in the electrolysis of a sodium chloride solution is the production of chlorine at the anode while in an alkali solution, the cathode reaction results in the formatting of hydrogen gas and hydroxide ions.²⁶⁹

Anode:
$$2Cl^{-} \rightarrow Cl_2 + 6H^{+} + 6e^{-}$$
 (21)

Cathode:
$$6H^+ + 6e^- \rightarrow 3H_2$$
 (22)

It is possible to collect hydrogen gas by separating the anode and cathode reaction products so that they do not react. Other electrolyses of sodium chloride, depending on the circumstances, can generate substances such sodium hypochlorite, chlorate, and perchlorate in addition to hydrogen (at the cathode):

$$NaCl + H_2O \rightarrow NaOCl + H_2$$
 (Overall hypochlorite reaction) (23)

$$NaCl + H_2O + Cl_2 \rightarrow NaOCl_3 + H_2$$
 (Overall chlorate reaction) (24)

$$NaCl + H_2O + 3/2Cl_2 \rightarrow NaOCl_4 + H_2$$
 (Overall perchlorate reaction) (25)

The counter electrode additionally produces hydrogen at the cathode as a result of other inorganic synthesis.¹⁵

5. Sustainability of Hydrogen Production

Methods for producing hydrogen are based on seven criteria for sustainability. The first two criteria that need to be looked into have to do with how effectively hydrogen can be produced in accordance with the first and second laws of thermodynamics. Energy efficiency is determined by the first law of thermodynamics, while the second law emphasizes energy efficiency. Since efficiency is typically defined as the desired output divided by the required input, the following equation represents energy efficiency:

$$\eta = \frac{\text{mLHV}}{E_{\text{in}}} \tag{26}$$

Here, "m" represents the rate of hydrogen generation in kg/s, "LHV" represents the lower heating value of hydrogen (calculated as 121 MJ/kg), and "E_{in}" denotes the rate of energy consumption in MJ/kg. It is possible to transform the energy efficiency equation into the exergy efficiency equation as follows:

$$\psi = \frac{^{\text{mEx}_{\text{H}_2}^{\text{ch}}}}{^{\text{Ex}_{\text{in}}}} \tag{27}$$

 $Ex_{H_2}^{ch}$ stands for the chemical exergy of hydrogen in the exergy efficiency equation, and " Ex_{in} " stands for the rate of exergy input into the process. The energy and exergy efficiencies of the chosen hydrogen production technologies are taken from the literature for this study.²⁷⁰⁻²⁷²

The cost of producing hydrogen is the third factor, and it is crucial, especially when scaling up and commercializing processes. Making sustainable hydrogen more accessible and extensively used

on the market is a crucial first step. The least expensive methods for producing hydrogen right now are coal gasification and natural gas reforming, but they also produce the most pollutants. Technologies for carbon capture (CC) can lower the emissions. However, CC pushes up the price of producing hydrogen by 10% to 20%.²⁷³

The majority of renewable-based hydrogen production methods are still in their development as compared to conventional, fossil-based solutions. As a result, renewable hydrogen has a greater lifecycle cost than fossil-based hydrogen. However, the price of hydrogen derived from renewable sources has significantly reduced. Due to advancements in materials science and system designs, further cost reductions are anticipated for the majority of upcoming renewable hydrogen production techniques. While renewable hydrogen becomes more reasonably priced on a big scale, fossil-based hydrogen produced through carbon capture can be used as a bridge fuel. The cost information for the chosen hydrogen production technologies is gathered.^{20, 271, 274-276}

The probable effects of acidification and global warming according to the life cycle assessment (LCA) make up the fourth and fifth criteria. The LCA method is dependable for determining the true environmental effect.²⁷⁷ GWP measures the amount of CO₂ emissions compared to the amount of H₂ produced. Acidification potential (AP) measures the amount of waste that is discharged into the land and water in grams of SO_x per kilogram of H₂ generated. The two environmental impact metrics that are most frequently employed are GWP and AP.²⁷⁸ According to the literature, renewable hydrogen has a distinct advantage over fossil-based hydrogen in terms of GWP and AP.²⁷⁰, ²⁷¹, ²⁷³, ²⁷⁹

Cost of carbon (CC) is the sixth criterion. According to the harm done to the environment and human health, CC calculates the marginal external cost of a unit of CO₂ emissions. The literature has detailed descriptions of the many models used in the calculation of CC.²⁸⁰⁻²⁸⁴ The seventh criterion, known as the technology maturity level (TML), is rated on a modified, consolidated scale between 1 and 10. The TML facilitates the communication of a technology's maturity level. With regard to unique and small-scale alternatives, the grade 1 denotes the extremely early stages of research, and the number 10 denotes complete market integration. Data on the state of technology maturity are taken from Reference.²⁷²

All performance factors are standardized and ranked between 0 and 10 in the final step to carry out the comparison assessment. The optimal choice is 10, whereas the least desired scenario is 0. The technology maturity level is already on a 0–10 scale, where 0 and 10 represent the least and most preferable solutions, respectively, therefore there is no normalization added to it. The chosen hydrogen production techniques perform more sustainably across the board as their score rises from 0 to 10. Efficiency measures for energy and exergy are normalized by:

$$Rank(i) = efficiency(i) \times 10$$
 (28)

The remaining factors (cost of manufacturing, cost of carbon, and potentials for global warming and acidification) are normalized appropriately and ordered as

$$Rank(i) = \frac{\max value - performance(i)}{\max value} \times 10$$
 (29)

Here, the chosen approach is represented by (i). The highest value in the related performance category is indicated by the term "max value" in equation (29). For example, if a method has the greatest emissions among the options chosen, it receives a score of 0. As an alternative, the option with the highest rating would be the one with the lowest cost. It should be highlighted that zero cost and emissions receive rating 10. No method receives the highest ranking as a result. This strategy seeks to demonstrate that each alternative still has room for improvement across all chosen performance metrics. Each of the chosen hydrogen generation solutions is given a total sustainability score after all performance parameters have been normalized and graded between 0 and 10. The overall scores are compared to the ideal hypothetical case where hydrogen is produced with 100 percent energy and exergy efficiency, zero GWP, AP, and cost, and a TML of ten. The average scores are then determined. **Table 7** illustrates detailed sustainability performance rankings of the selected hydrogen production methods. The eight cases used to determine average scores are as follows:²¹⁰

EI: All factors are equally important.

EE: energy efficiency is given a 40% weighting, and the remaining criteria are each given a 10% weighting.

ExE: exergy efficiency is given a 40% weighting, and the remaining criteria are each given a 10% weighting.

CC: The weight for the cost of carbon is 40%, and the remaining criteria are each given a 10% weight.

Cost: Production cost is given a 40% weighting, while the remaining criteria are each given a 10% weighting.

AP: AP is given a 40% weighting, and the remaining criteria are each given a 10% weighting.

GWP: The weight for GWP is 40%, and the remaining criteria are each given a 10% weight.

TML: TML is given a 40% weighting, and the remaining criteria are each given a 10% weighting.

Table 7:Detailed sustainability performance rankings of the selected hydrogen production methods in different cases and the hypothetical ideal case²¹⁰

	EI	$\mathbf{E}\mathbf{E}$	ExE	CC	Cost	AP	GWP	TML
Electrolysis(large scale)	7.7	7.7	6.5	8.3	7.1	8.1	8.3	8.1
PV electrolysis	4.6	3.6	3.4	5.6	3.5	5.5	5.6	4.7
High temperature electrolysis	6.3	6.9	5.5	6.9	5.2	7.0	6.9	5.6
Photoelectrochemical cell	4.8	3.6	3.4	6.3	3.4	6.3	6.3	4.6
Ideal	10.0	10.0	10.0	10.0	10.0	10.0	10.0	10.0

In the twenty-first century, sustainable energy systems are expected to play significant roles in the supply and demand aspects of the use of current sources. Identification of dependable, economical, plentiful, and clean sources for H_2 production area necessity. There is a much work being done to create and improve systems that manufacture H_2 more cheaply from renewable resources in order to further reduce emissions and energy use.

Hydrogen is widely regarded as an environmentally friendly secondary source of renewable energy and a viable replacement for fossil fuels because it is the only fuel that is carbon-free and has the largest energy density of any fuel known.²⁸⁵⁻²⁸⁷ Another benefit is that hydrogen can be used for domestic consumption and can be safely transported using conventional transportation methods.²⁸⁸⁻²⁹¹ It can also be stored as compressed gas, cryogenic liquid, or solid hydride in order to be fed to stationary fuel cells.²⁹²⁻²⁹⁴ A minor portion is utilisation in cars, and applications such

as power generation and heating in the residential and industrial sectors are anticipated in the near future. ^{290, 295, 296}

The cost of alternative energy sources and novel H₂ generation techniques is falling, while the effectiveness of H₂ based energy conversion systems is rising. H₂ is therefore anticipated to achieve future sustainability objectives.²⁹⁷ Options for electrolysis based on photovoltaics are also thought to be viable for producing hydrogen sustainably.²⁰ Unfortunately, the low conversion efficiency and the high investment costs are major barriers to the competitiveness of water splitting technologies compared to conventional approaches. Integrating storage, transportation, and hydrogen generation based on renewable energy sources is essential for sustainable hydrogen production.²⁹⁸ Hydrogen must be produced in clean, dependable, cost-effective, and safe ways that do not harm society or the environment in order for hydrogen systems to be acceptably sustainable. The following important factors should be taken into account:

- Technical performance (energy efficiencies, process control, raw material input),
- Social performance (impact on public health, employment and training opportunities, and public acceptance),
- Environmental performance (greenhouse gas emissions, land use, water discharge quality, and solid waste), and
- Availability/reliability (dependence on imported resources, predictability, and scalability).

Grid electrolysis (electricity from fossil fuels), wind electrolysis, solar electrolysis, nuclear thermochemical water splitting cycles, solar thermochemical water splitting cycles, and photoelectrochemical cells are some of the current and prospective hydrogen generation technologies. Grid electrolysis is anticipated to hold the key to more environmentally friendly hydrogen production in the near future as other technologies develop and their costs come down. In the long run, wind electrolysis and solar thermochemical water splitting cycles will be promising methods for producing sustainable hydrogen.²⁹⁹ Research into new, better performing (ideally abundant) materials is necessary to enable all of these technologies to attain greater sustainability while aiming for cost reduction. A possible route to 100% sustainably produced hydrogen in the energy sector is shown in **Fig 28**



Fig 28: A potential pathway to reach 100% sustainable hydrogen in the energy market. Modified from ref. ²¹⁰ with permission from [Elsevier], copyright [2022].

6. Hydrogen Economy

The cost of feedstock, the efficiency of the technology used, the stage of development (e.g., early stage or mature), and the physical proximity to end use markets (centralized or distributed production) are just a few of the many factors that affect the economics of hydrogen production. Investment costs play a large role in determining hydrogen production costs. The production strategy and plant size have an impact on the cost structure. For instance, the fuel cost share ranges from 50 to 68% in large-scale SMRs while it is only between 28 and 40% in small reformer units. Electricity costs account for between 75 and 80 percent of the cost of electrolytic hydrogen. Fuel costs for biomass gasification are roughly 40%. Regarding the evolution of feedstock prices, natural gas is forecast to cost more during the following ten years, while coal is anticipated to cost the same. Costs of electricity are significantly influenced by changes in the price of feedstocks, particularly fossil fuels.

A cheap and sustainable source of hydrogen is necessary for the Hydrogen Economy to succeed in the future. Presently, fossil fuels like coal and natural gas are mostly used to produce hydrogen. However, the availability of both of these fuels is constrained, and the creation of hydrogen results in the release of greenhouse gases. Therefore, in order to produce hydrogen in a hydrogen economy, alternative energy sources must be investigated for both environmental and economic reasons. The cost of operating fossil fuel facilities is rising, whereas the cost of alternative energy technology is falling as economies of scale are reached, even if historically the cost of hydrogen from fossil fuel plants has been less expensive than that from other energy sources. In the

electrochemical production of hydrogen, the cost of producing hydrogen using the existing light water reactors with electrolysis is greater and is anticipated to range from 4.36 to 7.36 \$/kg, which would not be regarded as a low-cost energy source in light of current gasoline prices.²² Costs for electrochemical methods of producing hydrogen are shown in **Table 8**.¹⁵ The projected costs for PEM electrolysis and SOE to produce hydrogen are now \$5.25/ kg and \$4.7/ kg, respectively. According to future predictions, using electricity generated from renewable resources, electrolysis-produced hydrogen will cost *ca.* \$2/ kg. The cost of solar thermochemical hydrogen is approximately \$2.5/ kg. Currently, there are roughly 0.1 GT of hydrogen produced annually, most of which is used locally to produce ammonia or to refine and treat metals.^{286, 295}

Table 8: Representative costs for electrochemical hydrogen production methods. ¹⁵

Electrochemical Hydrogen production methods	Production costs \$/ kg of H ₂
SOE electrolysis	4.7–3.8 (forecast)
PEM electrolysis	5.25–4.5 (forecast)
Solar electrolysis	2.0

Compared to other methodologies, creating hydrogen gas with wind and solar energy is more expensive. This scenario is the result of a number of economic and technological variables, including the cost of maintenance work, the technology used in power systems, and the price of electricity generated by wind and solar systems. The high expenses of distributed and small-scale manufacturing in comparison to the industrial size of conventional power facilities is another factor. Unfortunately, carbon-based conversion is the most cost-effective way for producing hydrogen (steam methane reforming, coal and biomass gasification). Although many people believe that nuclear energy can produce hydrogen at a scale that is economically viable, there are still a number of restrictions and technical issues that need to be resolved.³⁰¹

The overall system has a significant impact on the efficiency of the conversion from electricity to hydrogen and back to electricity. The efficiency of hydrogen production from low temperature electrolysis will be no higher than 25%. However, by switching from low to high temperature electrolysis, which produces steam at 800°C, and by using advanced nuclear plants with higher thermal-to-electric conversion efficiencies, this conversion might be increased.³⁰²

Table 9: Electrical and thermal efficiencies of conversion for different hydrogen production routes³⁰³⁻³⁰⁶

Conversion routes	Conversion efficiency (%)
Nuclear heat + electrolysis	28
Wind + electrolysis	70
Solar PV + electrolysis	10.5
Hydroelectric + electrolysis	70
Tidal + electrolysis	70

Examples of the technical, economic, and environmental aspects of systems for producing hydrogen using fossil and non-fossil fuels may be found widely in the literature. ^{270, 271}For instance, Dawood et al. ²⁷²have examined function of hydrogen in future energy systems and suggested a pathway toward 100% renewable energy systems. The current situation of the hydrogen supply chain is depicted as an advancing energy vector in the techno-economic assessment of hydrogen production methods, which includes resources, generating and storage technologies, demand market, and economics. Ji and Wang have studied the state-of-the-art, most recent developments, and difficulties of both fossil- and renewable-based hydrogen production techniques. They have come to the conclusion that electrolysis and thermochemical cycles in combination with renewable energy sources exhibit significant economic and environmental promise. ²⁷³

Table 10: Production cost and final cost for hydrogen from different processes^{275, 307-309}

Process hydrogen from	Production mode	Cost (€/GJ)				
		Feedstock	Production	Final (incl. storage,		
				delivery, dispensing)		
Coal gasification	centralized	1.2	13–16	32–37		
Methane reforming	centralized (3 M	3	5–8	22–30		
	Nm^3/d)					
Biomass gasification	intermediate	2.4	17–22	33–40		
Methane reforming	decentralized	4–5	7–12	28–33		
Gasoline	refinery	2.5	6	7		
Electrolysis	decentralized	14	20–25	35–40		

Conclusion

The majority of the remaining hydrogen produced today comes via electrolysis of water, with the remaining 95% coming from hydrocarbons often reacting with steam. In order to produce

hydrogen from non-fossil natural resources in substantial amounts, a hydrogen-based energy system will need to rely on low-cost and effective methods. Using electrolysis, which primarily uses renewable energy sources and water, accounts for only 4% of global hydrogen production. The amounts of hydrogen needed are enormous and orders of magnitude more than what is now produced, according to estimates from different nations. Splitting water, which is a perfect hydrogen transporter, is the most sustainable method of obtaining hydrogen. Hydrogen and oxygen are split from water by electrolysis, a practical and proven process that today yields very pure hydrogen for usage in the electronics, pharmaceutical, and food sectors. Due to the fact that water electrolysis only necessitates a modest amount of storage, it is a safe choice for producing hydrogen at the point of use in relatively small quantities. Around 80% of the cost of producing hydrogen comes from the electricity needed to electrolyse water and separate it into hydrogen and oxygen. Potentially, electrolysis can produce a clean and renewable energy supply when combined with a renewable energy source. However, electrolysis by itself would not be able to produce all the hydrogen anticipated to be required for upcoming energy demands. Although pilot systems are being investigated, the use of solar radiation for heating and/or photocatalysis shows considerable promise but still needs further research and development. This is currently being conducted on photoelectrochemical catalysts that create hydrogen when exposed to visible light in order to increase their robustness, efficiency, and material costs. There are many choices of methods of producing hydrogen that might be sustainable and prevent this consumption of fossil fuels. However, for them to develop there must be both significant capital investments in the infrastructure and political legislation-driven incentive. Different electrochemical methods have been discussed in detail in this study including wind, solar and nuclear assisted water electrolysis, high and low temperature water electrolysis, electrolysis using organic fuels and hydrogen production as a by-product of various electrolytic methods. This review makes an effort to do just that while also going detailing the economics and status of industrial and development electrolysis.

Future Perspectives

In general, electrolysis is regarded a well-known alternative technique for producing hydrogen that has already attained a significant market potential. Megawatt scale units are already available, and problems with project production and supply chain development are also being addressed.

Between the years 2020–2025 electrolysis is expected to become a marketable technology. The systems' durability is now a limitation of electrolysis technology, however, owing to intensive research, these issues should be solved in the upcoming decades. The viability will depend on the cost of the required renewable electricity. There are several future perspectives which are given below:

1. Resolving Durability Challenges

One of the primary challenges facing electrolysis technology is the durability of the systems. However, through extensive research and development efforts, it is anticipated that these difficulties will be overcome in the coming decades. This improvement in durability is a critical step in making electrolysis a more reliable and long-lasting technology.

2. Cost-Effective Hydrogen Production

The viability of electrolysis for hydrogen production is closely tied to the cost of renewable electricity. As renewable energy sources become more accessible and affordable, the cost-effectiveness of electrolysis is expected to increase. This shift is particularly significant as we strive to reduce carbon emissions and transition to a cleaner energy landscape.

3. Advancements in Solid Oxide Electrolysis (SOE)

Solid Oxide Electrolysis (SOE) systems are poised to become more economical and durable in the next decade. They are expected to catch up with traditional alkaline and PEM electrolysis technologies by 2030. This advancement in SOE technology will contribute to a more diverse and competitive hydrogen production landscape.¹⁶⁴

4. Nuclear-Powered Hydrogen Production

A prospective approach involves utilizing electrolytically produced hydrogen derived from nuclear power sources. This method enables the generation and storage of hydrogen during periods of low electrical demand, which can then be converted back into energy during peak demand. As natural gas prices rise, the stability of nuclear power steam generation becomes increasingly attractive, offering a reliable alternative for hydrogen production.³¹⁰

5. Carbon-Neutral Hydrogen Production

The quest for cost-effective hydrogen production without emitting carbon dioxide remains a top priority. As technology continues to advance, there is a strong possibility that we will achieve the goal of producing hydrogen in an environmentally friendly and economically viable manner. The recent developments in this area are highlighted.²¹⁰

6. Underground Seasonal Hydrogen Storage (USHS)

To secure the energy supply chain for a hydrogen-based future, large-scale energy storage technologies are essential. Underground Seasonal Hydrogen Storage (USHS) is emerging as a viable method to address the temporal fluctuations in renewable energy output. Geological research, including assessments of geochemical and biological reactions, is critical to its success. The connection between hydrogen demand and various applications, such as ammonia generation and integration into power systems, will shape the future energy landscape.³¹¹

7. Collaboration and Diverse Production Technologies

Collaboration between government agencies, industry leaders, and educational institutions is crucial for driving advancements in hydrogen production. Both centralized and decentralized methods of hydrogen production are under investigation. Prioritizing the improvement of existing commercial methods, while also exploring cutting-edge technologies such as direct photon-to-hydrogen energy-based water splitting, will lead to diverse and efficient production configurations.

8. Policy Adjustments and Technological Advancements

To achieve these goals, several steps and policy adjustments are recommended: 14

- Foster Technology and Market Development: Government support should prioritize the development of carbon dioxide capture and absorption technologies and the advancement of renewable and low-carbon-emitting methods.
- ii. **Improve Gas Separation and Purification Techniques:** Research into high-efficiency hydrogen purification technologies suitable for distributed reformers is essential.
- iii. **Invest in Small Reformers:** Utilizing small reformers powered by various fuels can reduce the cost of hydrogen supply, with a focus on reliability and compatibility with fuel cells.

- iv. Reduce Electrolyzer Expenses and Maximize Efficiency: Continuous improvement in electrolyzer efficiency and cost reduction is vital, especially for decentralized power generation.
- v. **Explore Innovative Photolytic Processes:** Advancements in photolytic processes that use light energy for hydrogen production should be a research priority, with a focus on efficiency and corrosion resistance.
- vi. **Nuclear-Powered Hydrogen:** Develop cost-effective and environmentally friendly methods for producing hydrogen from nuclear energy, leveraging advanced nuclear reactor technology.
- vii. **Carbon Dioxide Collection and Sequestration:** Integrate carbon dioxide capture systems into hydrogen production plants to minimize carbon emissions.
- viii. **Demonstrations and Technology Integration:** Showcase hydrogen production technology alongside practical examples to generate market interest and promote safety.
- ix. **Large-Scale Testing Sites:** Establish dedicated sites for large-scale testing and technology display to address logistical challenges.

In conclusion, the future of hydrogen production through electrolysis is bright, with a range of advancements on the horizon. Through collaborative efforts, technological innovation, and policy support, we can build a reliable and efficient hydrogen production system that plays a pivotal role in a sustainable energy future.

Acknowledgements

Support from the Cardiff University to Dr. Nisar Ahmed is gratefully acknowledged.

Conflict of Interest

The authors declare no conflict of interest.

References

- 1. R. A. Hites, *Persistent organic pollutants in the Great Lakes*, 2005, 1-12.
- 2. H. Lund, energy, 2007, **32**, 912-919.
- 3. K. Blok, Energy Policy, 2005, **33**, 1635-1641.

- 4. J. Turner, G. Sverdrup, M. K. Mann, P. C. Maness, B. Kroposki, M. Ghirardi, R. J. Evans and D. Blake, *International journal of energy research*, 2008, **32**, 379-407.
- 5. K. T. Møller, T. R. Jensen, E. Akiba and H.-w. Li, *Progress in Natural Science: Materials International*, 2017, **27**, 34-40.
- 6. J.-S. Kim, D.-C. Lee, J.-J. Lee and C.-W. Kim, *Scientific reports*, 2020, **10**, 15586.
- 7. M. Ball and M. Weeda, *International Journal of Hydrogen Energy*, 2015, **40**, 7903-7919.
- 8. I. Staffell, D. Scamman, A. V. Abad, P. Balcombe, P. E. Dodds, P. Ekins, N. Shah and K. R. Ward, *Energy & Environmental Science*, 2019, **12**, 463-491.
- 9. G. E. Badea, C. Hora, I. Maior, A. Cojocaru, C. Secui, S. M. Filip and F. C. Dan, *Energies*, 2022, **15**, 8560.
- 10. B. Ewan and R. Allen, *International Journal of Hydrogen Energy*, 2005, **30**, 809-819.
- 11. C. M. Kalamaras and A. M. Efstathiou, 2013.
- 12. M. H. Islam, O. S. Burheim and B. Pollet, 2018.
- 13. J. J. Lamb, M. Hillestad, E. Rytter, R. Bock, A. S. Nordgård, K. M. Lien, O. S. Burheim and B. G. Pollet, in *Hydrogen, biomass and bioenergy*, Elsevier, 2020, pp. 21-53.
- 14. C. Acar and I. Dincer, *Comprehensive energy systems*, 2018, **3**, 1-40.
- 15. K. Scott, *Electrochemical Methods for Hydrogen Production*, 2019, **25**, 392.
- 16. F. H. Sobrino, C. R. Monroy and J. L. H. Pérez, *Renewable and Sustainable Energy Reviews*, 2010, **14**, 772-780.
- 17. I. Dincer, *International journal of hydrogen energy*, 2012, **37**, 1954-1971.
- 18. J. Turner, G. Sverdrup and M. Mann, *J. Energy Res*, 2008, **32**, 379.
- 19. S. S. Kumar and H. Lim, *Energy reports*, 2022, **8**, 13793-13813.
- 20. P. Nikolaidis and A. Poullikkas, *Renewable and sustainable energy reviews*, 2017, **67**, 597-611.
- 21. M. Balat and M. Balat, *International journal of hydrogen energy*, 2009, **34**, 3589-3603.
- J. R. Bartels, M. B. Pate and N. K. Olson, *International journal of hydrogen energy*, 2010,
 35, 8371-8384.
- 23. A. Midilli, H. Kucuk, M. E. Topal, U. Akbulut and I. Dincer, *International Journal of Hydrogen Energy*, 2021, **46**, 25385-25412.
- 24. F. Barbir, *Energy*, 2009, **34**, 308-312.

- 25. A. Ahmed, A. Q. Al-Amin, A. F. Ambrose and R. Saidur, *International journal of hydrogen energy*, 2016, **41**, 1369-1380.
- 26. M. F. Milazzo, F. Spina, P. Primerano and J. Bart, *Renewable and Sustainable Energy Reviews*, 2013, **26**, 579-624.
- 27. M. A. Khan, H. Zhao, W. Zou, Z. Chen, W. Cao, J. Fang, J. Xu, L. Zhang and J. Zhang, *Electrochemical Energy Reviews*, 2018, **1**, 483-530.
- 28. M. Bodner, A. Hofer and V. Hacker, *Wiley Interdisciplinary Reviews: Energy and Environment*, 2015, **4**, 365-381.
- 29. I. K. Kapdan and F. Kargi, Enzyme and microbial technology, 2006, 38, 569-582.
- 30. M. Ricci, G. Newsholme, P. Bellaby and R. Flynn, *International Journal of Energy Sector Management*, 2007, **1**, 34-50.
- 31. A. Demirbas, *Energy Sources, Part B: Economics, Planning, and Policy*, 2017, **12**, 172-181.
- 32. S. V. Mohan, Y. V. Bhaskar and P. Sarma, Water Research, 2007, 41, 2652-2664.
- 33. A. L. Ortiz, M. M. Zaragoza and V. Collins-Martínez, *International journal of hydrogen energy*, 2016, **41**, 23363-23379.
- 34. S. E. Hosseini and M. A. Wahid, *Renewable and Sustainable Energy Reviews*, 2016, **57**, 850-866.
- 35. M. Balat, Energy Sources, Part B: Economics, Planning, and Policy, 2007, 2, 49-61.
- 36. N. Z. Muradov and T. N. Veziroğlu, *International journal of hydrogen energy*, 2005, **30**, 225-237.
- 37. A. Ajanovic, M. Sayer and R. Haas, *International Journal of Hydrogen Energy*, 2022, **47**, 24136-24154.
- 38. M. Newborough and G. Cooley, Fuel Cells Bulletin, 2020, 2020, 16-22.
- 39. M. Noussan, P. P. Raimondi, R. Scita and M. Hafner, Sustainability, 2020, 13, 298.
- 40. Z. Navas-Anguita, D. García-Gusano, J. Dufour and D. Iribarren, *Science of the total Environment*, 2021, 771, 145432.
- 41. A. M. Amin, E. Croiset and W. Epling, *International Journal of Hydrogen Energy*, 2011, **36**, 2904-2935.
- 42. M. Carmo, D. L. Fritz, J. Mergel and D. Stolten, *International journal of hydrogen energy*, 2013, **38**, 4901-4934.

- S. Zhiznin, V. Timokhov and A. Gusev, *International Journal of Hydrogen Energy*, 2020,
 45, 31353-31366.
- 44. A. Konieczny, K. Mondal, T. Wiltowski and P. Dydo, *International Journal of Hydrogen Energy*, 2008, **33**, 264-272.
- 45. S. Wang, A. Lu and C.-J. Zhong, *Nano Convergence*, 2021, **8**, 1-23.
- 46. M. Rashid, M. K. Al Mesfer, H. Naseem and M. Danish, *International Journal of Engineering and Advanced Technology*, 2015.
- 47. C. Hora, F. C. Dan, N. Rancov, G. E. Badea and C. Secui, *Energies*, 2022, **15**, 6076.
- 48. L. Pérez Orosa, E. Chinarro, D. Guinea and M. C. García-Alegre, *Energies*, 2022, **15**, 5888.
- 49. B. Jenkins, D. Squires, J. Barton, D. Strickland, K. Wijayantha, J. Carroll, J. Wilson, M. Brenton and M. Thomson, *Energies*, 2022, **15**, 5796.
- 50. A. Saravanan, S. Karishma, P. S. Kumar, P. Yaashikaa, S. Jeevanantham and B. Gayathri, *Biomass Conversion and Biorefinery*, 2020, 1-21.
- 51. A. M. Elgarahy, M. Eloffy, A. Hammad, A. N. Saber, D. M. El-Sherif, A. Mohsen, M. Abouzid and K. Z. Elwakeel, *Environmental Chemistry Letters*, 2022, **20**, 3453-3504.
- 52. S. M. Saba, M. Müller, M. Robinius and D. Stolten, *International journal of hydrogen energy*, 2018, **43**, 1209-1223.
- 53. Y. Liu, F. Wang, Z. Jiao, S. Bai, H. Qiu and L. Guo, *Electrochemical Energy Reviews*, 2022, **5**, 5.
- 54. J. Wang, Z. Zhang, J. Ding, C. Zhong, Y. Deng, X. Han and W. Hu, *Science China Materials*, 2021, **64**, 1-26.
- 55. H.-Y. Wang, C.-C. Weng, J.-T. Ren and Z.-Y. Yuan, *Frontiers of Chemical Science and Engineering*, 2021, 1-19.
- 56. D. V. Esposito, Joule, 2017, 1, 651-658.
- 57. M. Gong, D.-Y. Wang, C.-C. Chen, B.-J. Hwang and H. Dai, *Nano Research*, 2016, **9**, 28-46.
- 58. X. Li, L. Zhao, J. Yu, X. Liu, X. Zhang, H. Liu and W. Zhou, *Nano-Micro Letters*, 2020, 12, 1-29.
- 59. S. Atilhan, S. Park, M. M. El-Halwagi, M. Atilhan, M. Moore and R. B. Nielsen, *Current Opinion in Chemical Engineering*, 2021, **31**, 100668.
- 60. F. Mödinger, Interceram-International Ceramic Review, 2021, 70, 32-37.

- 61. B. S. Thapa and B. Thapa, 2020.
- Y. Zhao, V. McDonell and S. Samuelsen, *International Journal of Hydrogen Energy*, 2020,
 45, 11368-11379.
- 63. H. Balat and E. Kırtay, *International journal of hydrogen energy*, 2010, **35**, 7416-7426.
- 64. L. Hu, G. r. Lindbergh and C. Lagergren, *The Journal of Physical Chemistry C*, 2016, **120**, 13427-13433.
- 65. L. Barelli, G. Bidini, G. Cinti and J. Milewski, *International Journal of Hydrogen Energy*, 2021, **46**, 14922-14931.
- 66. D. Penchini, G. Cinti, G. Discepoli and U. Desideri, *International journal of hydrogen energy*, 2014, **39**, 9457-9466.
- 67. A. Monforti Ferrario, F. Santoni, M. Della Pietra, M. Rossi, N. Piacente, G. Comodi and L. Simonetti, *Frontiers in Energy Research*, 2021, **9**, 655915.
- 68. S. Dresp, T. N. Thanh, M. Klingenhof, S. Brückner, P. Hauke and P. Strasser, *Energy & Environmental Science*, 2020, **13**, 1725-1729.
- 69. G. E. Badea, I. Maior, A. Cojocaru and I. Corbu, 2007.
- 70. A. Cojocaru, G. E. Badea, I. Maior, P. CREŢ and T. Badea, *Revue Roumaine de Chimie*, 2009, **54**, 49-54.
- 71. G. E. Badea, I. Maior, A. Cojocaru, I. Pantea and T. Badea, *Revue Roumaine de Chimie*, 2009, **54**, 55-61.
- 72. W. Zang, T. Sun, T. Yang, S. Xi, M. Waqar, Z. Kou, Z. Lyu, Y. P. Feng, J. Wang and S. J. Pennycook, *Advanced Materials*, 2021, **33**, 2003846.
- 73. V. V. Kuznetsov, B. I. Podlovchenko, K. V. Frolov, M. A. Volkov and D. A. Khanin, *Journal of Solid State Electrochemistry*, 2022, **26**, 2183-2193.
- 74. S. Farhangi, S. Ebrahimi and M. S. Niasar, *Biotechnology letters*, 2014, **36**, 1987-1992.
- 75. S. H. Hsu, J. Miao, L. Zhang, J. Gao, H. Wang, H. Tao, S. F. Hung, A. Vasileff, S. Z. Qiao and B. Liu, *Advanced Materials*, 2018, **30**, 1707261.
- 76. C. Zhang, D. Li and Y. Xu, Journal of Materials Research, 2022, 37, 807-817.
- 77. Z. Chen, D. Liu, Y. Gao, Y. Zhao, W. Xiao, G. Xu, T. Ma, Z. Wu and L. Wang, *Sci. China Mater.*, 2022, **65**, 1217-1224.
- 78. Q. Xiong, X. Zhang, Q. Cheng, G. Liu, G. Xu, J. Li, X. Ye and H. Gao, *Nano Research*, 2021, **14**, 1443-1449.

- 79. H. Xie, C. Lan, B. Chen, F. Wang and T. Liu, *Nano Research*, 2020, **13**, 3321-3329.
- 80. L. Dong, G.-R. Chang, Y. Feng, X.-Z. Yao and X.-Y. Yu, *Rare Metals*, 2022, 1-12.
- 81. J. Li, M. Song, Y. Hu, C. Zhang, W. Liu, X. Huang, J. Zhang, Y. Zhu, J. Zhang and D. Wang, *Nano Research*, 2023, **16**, 3658-3664.
- 82. G. Wang, Y. Sun, Y. Zhao, Y. Zhang, X. Li, L. Fan and Y. Li, *Nano Research*, 2022, **15**, 8771-8782.
- 83. Y. Chen, P. Sun and W. Xing, Journal of Chemical Sciences, 2019, 131, 1-8.
- 84. D. Liang, Y. Liu, S. Peng, F. Lan, S. Lu and Y. Xiang, Frontiers of Environmental Science & Engineering, 2014, 8, 624-630.
- 85. Q. Yu, J. Chi, G. Liu, X. Wang, X. Liu, Z. Li, Y. Deng, X. Wang and L. Wang, *Science China Materials*, 2022, **65**, 1539-1549.
- 86. Q. Liu, S. Sun, L. Zhang, Y. Luo, Q. Yang, K. Dong, X. Fang, D. Zheng, A. A. Alshehri and X. Sun, *Nano Research*, 2022, **15**, 8922-8927.
- 87. C. González-Buch, I. Herraiz-Cardona, E. Ortega, J. García-Antón and V. Pérez-Herranz, *Journal of Applied Electrochemistry*, 2016, **46**, 791-803.
- 88. A. Laszczyńska and I. Szczygieł, *International Journal of Hydrogen Energy*, 2020, **45**, 508-520.
- 89. S. Wang, M. Wang, Z. Liu, S. Liu, Y. Chen, M. Li, H. Zhang, Q. Wu, J. Guo and X. Feng, *ACS Applied Materials & Interfaces*, 2022, **14**, 15250-15258.
- 90. L. Yu, L. Wu, S. Song, B. McElhenny, F. Zhang, S. Chen and Z. Ren, *ACS Energy Letters*, 2020, **5**, 2681-2689.
- 91. H. Li, Q. Tang, B. He and P. Yang, Journal of Materials Chemistry A, 2016, 4, 6513-6520.
- 92. J. Zheng, Y. Zhao, H. Xi and C. Li, RSC advances, 2018, 8, 9423-9429.
- 93. S. Gao, G.-D. Li, Y. Liu, H. Chen, L.-L. Feng, Y. Wang, M. Yang, D. Wang, S. Wang and X. Zou, *Nanoscale*, 2015, **7**, 2306-2316.
- 94. X. Wu, S. Zhou, Z. Wang, J. Liu, W. Pei, P. Yang, J. Zhao and J. Qiu, *Advanced Energy Materials*, 2019, **9**, 1901333.
- 95. J. Miao, Z. Lang, X. Zhang, W. Kong, O. Peng, Y. Yang, S. Wang, J. Cheng, T. He and A. Amini, *Advanced Functional Materials*, 2019, **29**, 1805893.
- 96. Y. Zhao, B. Jin, Y. Zheng, H. Jin, Y. Jiao and S. Z. Qiao, *Advanced Energy Materials*, 2018, **8**, 1801926.

- 97. Y. Jiao, H. Yan, D. Wang, X. Wang, S. Xu, Y. Xie, A. Wu, L. Jiang, C. Tian and R. Wang, SCIENCE CHINA-MATERIALS, 2022, 65, 1225-1236.
- 98. A. R. Jadhav, A. Kumar, J. Lee, T. Yang, S. Na, J. Lee, Y. Luo, X. Liu, Y. Hwang and Y. Liu, *Journal of Materials Chemistry A*, 2020, **8**, 24501-24514.
- 99. Y. Zhao, B. Jin, A. Vasileff, Y. Jiao and S.-Z. Qiao, *Journal of materials chemistry A*, 2019, 7, 8117-8121.
- 100. L. Chen and J. Shi, Science China Materials, 2022, 65, 1-9.
- 101. J. Hnát, M. Paidar and K. Bouzek, in *Current Trends and Future Developments on (Bio-) Membranes*, Elsevier, 2020, pp. 91-117.
- 102. B. Dunn, H. Kamath and J.-M. Tarascon, Science, 2011, **334**, 928-935.
- 103. N. S. Lewis and D. G. Nocera, *Proceedings of the National Academy of Sciences*, 2006, **103**, 15729-15735.
- 104. I. Roger, M. A. Shipman and M. D. Symes, *Nature Reviews Chemistry*, 2017, 1, 0003.
- 105. R. Gao and D. Yan, *Advanced Energy Materials*, 2020, **10**, 1900954.
- 106. R. Gao, J. Zhu and D. Yan, *Nanoscale*, 2021, **13**, 13593-13603.
- 107. Z. Guo, W. Ye, X. Fang, J. Wan, Y. Ye, Y. Dong, D. Cao and D. Yan, *Inorganic Chemistry Frontiers*, 2019, **6**, 687-693.
- 108. X.-W. Lv, Z.-P. Hu, L. Chen, J.-T. Ren, Y.-P. Liu and Z.-Y. Yuan, ACS Sustainable Chemistry & Engineering, 2019, 7, 12770-12778.
- 109. Y. Zheng, Y. Jiao, A. Vasileff and S. Z. Qiao, *Angewandte Chemie International Edition*, 2018, **57**, 7568-7579.
- 110. J.-T. Ren, Y. Yao and Z.-Y. Yuan, *Green Energy & Environment*, 2021, **6**, 620-643.
- 111. M. A. Mushtaq, M. Arif, G. Yasin, M. Tabish, A. Kumar, S. Ibraheem, W. Ye, S. Ajmal, J. Zhao and P. Li, *Renewable and Sustainable Energy Reviews*, 2023, **176**, 113197.
- 112. M. A. Mushtaq, A. Kumar, G. Yasin, M. Arif, M. Tabish, S. Ibraheem, X. Cai, W. Ye, X. Fang and A. Saad, *Applied Catalysis B: Environmental*, 2022, **317**, 121711.
- 113. J.-W. Zhang, H. Zhang, T.-Z. Ren, Z.-Y. Yuan and T. J. Bandosz, *Frontiers of Chemical Science and Engineering*, 2021, **15**, 279-287.
- 114. J. Wang, S.-J. Kim, J. Liu, Y. Gao, S. Choi, J. Han, H. Shin, S. Jo, J. Kim and F. Ciucci, *Nature Catalysis*, 2021, **4**, 212-222.
- 115. J. Rossmeisl, A. Logadottir and J. K. Nørskov, Chemical physics, 2005, 319, 178-184.

- 116. C. C. Weng, J. T. Ren and Z. Y. Yuan, *ChemSusChem*, 2020, **13**, 3357-3375.
- 117. J.-T. Ren, Y.-J. Song and Z.-Y. Yuan, *Journal of Energy Chemistry*, 2019, **32**, 78-84.
- 118. J. A. Turner, *Science*, 2004, **305**, 972-974.
- 119. C. Xiang, K. M. Papadantonakis and N. S. Lewis, *Materials Horizons*, 2016, **3**, 169-173.
- M. Cuartero, G. Crespo, T. Cherubini, N. Pankratova, F. Confalonieri, F. Massa, M.-L. Tercier-Waeber, M. Abdou, J. r. Schäfer and E. Bakker, *Analytical chemistry*, 2018, 90, 4702-4710.
- 121. Z. Wang, Y. Gu and L. Wang, Frontiers in Energy, 2021, 15, 596-599.
- 122. F. Esmaeilion, Applied Water Science, 2020, 10, 84.
- 123. Y. Kuang, M. J. Kenney, Y. Meng, W.-H. Hung, Y. Liu, J. E. Huang, R. Prasanna, P. Li, Y. Li and L. Wang, *Proceedings of the National Academy of Sciences*, 2019, **116**, 6624-6629.
- 124. R. A. Evrin and I. Dincer, 2020.
- 125. A. Headley, G. Randolf, M. Virji and M. Ewan, *MRS Energy & Sustainability*, 2020, 7, E26.
- 126. F. Musharavati, P. Ahmadi and S. Khanmohammadi, *Journal of Thermal Analysis and Calorimetry*, 2021, **145**, 1673-1689.
- 127. S. Serag and A. Echchelh, *Technology and Economics of Smart Grids and Sustainable Energy*, 2022, 7, 30.
- 128. K. Meier, International Journal of Energy and Environmental Engineering, 2014, 5, 1-12.
- 129. Y. Gao, W. Yao, J. Wang and Z. Cui, *Journal of Thermal Science*, 2023, **32**, 93-108.
- 130. S. Rarotra, T. K. Mandal and D. Bandyopadhyay, Energy Technology, 2017, 5, 1208-1217.
- 131. M. R. Omidvar, A. H. Meghdadi Isfahani, R. Kumar, A. Mohammadidoust and A. Bewoor, *Biomass Conversion and Biorefinery*, 2021, 1-19.
- M. Rezaei, A. Mostafaeipour, M. Qolipour and M. Momeni, *Frontiers in Energy*, 2019,
 13, 539-550.
- 133. P. D. Cavaliere, A. Perrone and A. Silvello, *Metals*, 2021, **11**, 1816.
- 134. R. Banik and P. Das, *Journal of The Institution of Engineers (India): Series B*, 2020, **101**, 527-539.
- 135. S. Furfari and A. Clerici, *The European Physical Journal Plus*, 2021, **136**, 509.

- 136. S. Chai, G. Zhang, G. Li and Y. Zhang, *Clean Technologies and Environmental Policy*, 2021, 23, 1931-1946.
- 137. K. Jing, C. Liu, X. Cao, H. Sun and Y. Dong, *Journal of Electrical Engineering & Technology*, 2021, **16**, 2355-2365.
- 138. H. Niaz, M. M. Lakouraj and J. Liu, *Korean Journal of Chemical Engineering*, 2021, **38**, 1617-1630.
- 139. S. Rawat, B. Jha and M. K. Panda, *Iranian Journal of Science and Technology, Transactions of Electrical Engineering*, 2018, **42**, 403-417.
- 140. M. G. Shirkoohi, R. D. Tyagi, P. A. Vanrolleghem and P. Drogui, *Journal of Environmental Health Science and Engineering*, 2022, **20**, 1089-1109.
- 141. J. Brauns and T. Turek, *Processes*, 2020, **8**, 248.
- 142. L. Vidas and R. Castro, *Applied Sciences*, 2021, **11**, 11363.
- 143. O. Schmidt, A. Gambhir, I. Staffell, A. Hawkes, J. Nelson and S. Few, *International journal of hydrogen energy*, 2017, **42**, 30470-30492.
- 144. R. Vakulchuk, I. Overland and D. Scholten, *Renewable and sustainable energy reviews*, 2020, **122**, 109547.
- 145. M. Ingram, B. Baron and G. Janz, *Electrochimica Acta*, 1966, **11**, 1629-1639.
- 146. H. Bartlett and K. Johnson, Journal of The Electrochemical Society, 1967, 114, 457.
- 147. B. Kaplan, H. Groult, A. Barhoun, F. Lantelme, T. Nakajima, V. Gupta, S. Komaba and N. Kumagai, *Journal of The Electrochemical Society*, 2002, **149**, D72.
- 148. V. Kaplan, E. Wachtel, K. Gartsman, Y. Feldman and I. Lubomirsky, *Journal of the Electrochemical Society*, 2010, **157**, B552.
- 149. H. V. Ijije, C. Sun and G. Z. Chen, *Carbon*, 2014, **73**, 163-174.
- 150. H. V. Ijije, R. C. Lawrence, N. J. Siambun, S. M. Jeong, D. A. Jewell, D. Hu and G. Z. Chen, *Faraday discussions*, 2014, **172**, 105-116.
- 151. H. V. Ijije, R. C. Lawrence and G. Z. Chen, RSC advances, 2014, 4, 35808-35817.
- 152. D. Chery, V. Albin, V. Lair and M. Cassir, *international journal of hydrogen energy*, 2014, **39**, 12330-12339.
- 153. D. Chery, V. Lair and M. Cassir, Electrochimica Acta, 2015, 160, 74-81.
- 154. J. Ren, F.-F. Li, J. Lau, L. González-Urbina and S. Licht, *Nano letters*, 2015, **15**, 6142-6148.

- 155. J. Ren, J. Lau, M. Lefler and S. Licht, *The Journal of Physical Chemistry C*, 2015, **119**, 23342-23349.
- 156. J. P. Perez-Trujillo, F. Elizalde-Blancas, M. Della Pietra and S. J. McPhail, *Applied energy*, 2018, **226**, 1037-1055.
- 157. J. P. Pérez-Trujillo, F. Elizalde-Blancas, S. J. McPhail, M. Della Pietra and B. Bosio, *Applied Energy*, 2020, **263**, 114630.
- 158. L. Hu, I. Rexed, G. Lindbergh and C. Lagergren, *international journal of hydrogen energy*, 2014, **39**, 12323-12329.
- 159. E. Audasso, K. I. Kim, G. Accardo, H. S. Kim and S. P. Yoon, *Journal of Power Sources*, 2022, **523**, 231039.
- 160. W. Dönitz and E. Erdle, *International Journal of Hydrogen Energy*, 1985, **10**, 291-295.
- 161. A. Nechache and S. Hody, *Renewable and Sustainable Energy Reviews*, 2021, **149**, 111322.
- 162. Y. Zheng, Z. Chen and J. Zhang, Electrochemical Energy Reviews, 2021, 4, 508-517.
- 163. Y. Li, L. Zhang, B. Yu, J. Zhu and C. Wu, Engineering, 2023, 21, 101-114.
- 164. D. Guban, I. K. Muritala, M. Roeb and C. Sattler, *International Journal of Hydrogen Energy*, 2020, **45**, 26156-26165.
- 165. M. Schalenbach, A. R. Zeradjanin, O. Kasian, S. Cherevko and K. J. Mayrhofer, International Journal of Electrochemical Science, 2018, 13, 1173-1226.
- M. Wang, G. Wang, Z. Sun, Y. Zhang and D. Xu, Global Energy Interconnection, 2019,
 2, 436-443.
- 167. V. Romano, G. D'Angelo, S. Perathoner and G. Centi, *Energy & Environmental Science*, 2021, **14**, 5760-5787.
- 168. A. Ursúa Rubio, L. Gandía Pascual and P. Sanchis Gúrpide, *Proceedings of the IEEE, 100* (2), 2012, 2012.
- 169. Z. Liu, S. D. Sajjad, Y. Gao, H. Yang, J. J. Kaczur and R. I. Masel, *International Journal of Hydrogen Energy*, 2017, **42**, 29661-29665.
- 170. K. Zeng and D. Zhang, *Progress in energy and combustion science*, 2010, **36**, 307-326.
- 171. S. Marini, P. Salvi, P. Nelli, R. Pesenti, M. Villa, M. Berrettoni, G. Zangari and Y. Kiros, *Electrochimica Acta*, 2012, **82**, 384-391.
- 172. E. Bianco and H. Blanco, 2020.

- 173. D. Jones and C. W. Dunnill, 2021.
- 174. D. Pletcher and X. Li, International Journal of Hydrogen Energy, 2011, 36, 15089-15104.
- 175. M. R. Kraglund, D. Aili, K. Jankova, E. Christensen, Q. Li and J. O. Jensen, *Journal of The Electrochemical Society*, 2016, **163**, F3125.
- 176. S. H. Ahn, S. J. Yoo, H.-J. Kim, D. Henkensmeier, S. W. Nam, S.-K. Kim and J. H. Jang, *Applied Catalysis B: Environmental*, 2016, **180**, 674-679.
- 177. Y. Leng, G. Chen, A. J. Mendoza, T. B. Tighe, M. A. Hickner and C.-Y. Wang, *Journal of the American Chemical Society*, 2012, **134**, 9054-9057.
- 178. Z. Xu, C.-L. Yeh, J.-L. Chen, J. T. Lin, K.-C. Ho and R. Y.-Y. Lin, ACS Sustainable Chemistry & Engineering, 2022, 10, 11577-11586.
- 179. S. Liu, B. Li, S. V. Mohite, P. Devaraji, L. Mao and R. Xing, *International Journal of Hydrogen Energy*, 2020, **45**, 29929-29937.
- 180. L. Bertuccioli, A. Chan, D. Hart, F. Lehner, B. Madden and E. Standen, 2014.
- 181. S. S. Kumar and V. Himabindu, *Materials Science for Energy Technologies*, 2019, **2**, 442-454.
- 182. L. Nuttall, A. Fickett and W. Titterington, *Hydrogen Energy: Part A*, 1975, 441-455.
- 183. W. Grubb, Journal of the Electrochemical Society, 1959, 106, 275.
- 184. W. Grubb and L. Niedrach, Journal of the Electrochemical Society, 1960, 107, 131.
- 185. K. Ayers, N. Danilovic, K. Harrison and H. Xu, *The Electrochemical Society Interface*, 2021, **30**, 67.
- 186. W. Xu and K. Scott, *International Journal of Hydrogen Energy*, 2010, **35**, 12029-12037.
- 187. M. T. Giacomini, M. Balasubramanian, S. Khalid, J. McBreen and E. Ticianellia, *Journal of The Electrochemical Society*, 2003, **150**, A588.
- 188. C. Rozain, E. Mayousse, N. Guillet and P. Millet, *Applied Catalysis B: Environmental*, 2016, **182**, 153-160.
- 189. L. Yin, T. Yang, X. Ding, M. He, W. Wei, T. Yu and H. Zhao, *Electrochemistry Communications*, 2018, **94**, 59-63.
- 190. M. Bühler, P. Holzapfel, D. McLaughlin and S. Thiele, *Journal of The Electrochemical Society*, 2019, **166**, F1070.
- 191. E. V. dos Santos and O. Scialdone, in *Electrochemical Water and Wastewater Treatment*, Elsevier, 2018, pp. 239-266.

- 192. M. Sillanpaa and M. Shestakova, *Electrochemical water treatment methods:* Fundamentals, methods and full scale applications, Butterworth-Heinemann, 2017.
- 193. S. Z. Baykara, International Journal of Hydrogen Energy, 2018, 43, 10605-10614.
- 194. H. Ju, S. Badwal and S. Giddey, *Applied energy*, 2018, **231**, 502-533.
- 195. S. Grigoriev, P. Millet and V. Fateev, *Journal of Power Sources*, 2008, 177, 281-285.
- 196. J. B. Benziger, M. B. Satterfield, W. H. Hogarth, J. P. Nehlsen and I. G. Kevrekidis, *Journal of power sources*, 2006, **155**, 272-285.
- D. Li, E. J. Park, W. Zhu, Q. Shi, Y. Zhou, H. Tian, Y. Lin, A. Serov, B. Zulevi and E. D. Baca, *Nature Energy*, 2020, 5, 378-385.
- 198. G.-F. Li, M. Divinagracia, M. F. Labata, J. D. Ocon and P.-Y. Abel Chuang, *ACS applied materials & interfaces*, 2019, **11**, 33748-33758.
- 199. M. Manolova, C. Schoeberl, R. Freudenberger, C. Ellwein, J. Kerres, S. Stypka and B. Oberschachtsiek, *International journal of hydrogen energy*, 2015, **40**, 11362-11369.
- 200. A. Miller, L. Singh, L. Wang and H. Liu, Environment international, 2019, 126, 611-618.
- 201. J. Parrondo, C. G. Arges, M. Niedzwiecki, E. B. Anderson, K. E. Ayers and V. Ramani, *Rsc Advances*, 2014, **4**, 9875-9879.
- J. E. Park, S. Y. Kang, S.-H. Oh, J. K. Kim, M. S. Lim, C.-Y. Ahn, Y.-H. Cho and Y.-E.
 Sung, *Electrochimica Acta*, 2019, 295, 99-106.
- 203. C. C. Pavel, F. Cecconi, C. Emiliani, S. Santiccioli, A. Scaffidi, S. Catanorchi and M. Comotti, *Angewandte Chemie International Edition*, 2014, **53**, 1378-1381.
- I. Vincent, A. Kruger and D. Bessarabov, *International Journal of Hydrogen Energy*, 2017,42, 10752-10761.
- 205. I. Vincent, E.-C. Lee and H.-M. Kim, RSC advances, 2020, 10, 37429-37438.
- 206. I. Vincent and D. Bessarabov, *Renewable and Sustainable Energy Reviews*, 2018, **81**, 1690-1704.
- 207. D. Zhang and K. Zeng, *Industrial & Engineering Chemistry Research*, 2012, **51**, 13825-13832.
- 208. L. Wang, T. Weissbach, R. Reissner, A. Ansar, A. S. Gago, S. Holdcroft and K. A. Friedrich, *ACS Applied Energy Materials*, 2019, **2**, 7903-7912.
- 209. S. Dunn, International journal of hydrogen energy, 2002, 27, 235-264.
- 210. C. Acar and I. Dincer, international journal of hydrogen energy, 2022, 47, 40118-40137.

- 211. W. Brattain and C. Garrett, Bell System Technical Journal, 1955, 34, 129-176.
- 212. M. Grätzel, nature, 2001, 414, 338-344.
- 213. K. Kalyanasundaram, Solar Cells, 1985, 15, 93-156.
- 214. A. Fujishima and K. Honda, *nature*, 1972, **238**, 37-38.
- 215. F. A. Frame, E. C. Carroll, D. S. Larsen, M. Sarahan, N. D. Browning and F. E. Osterloh, *Chemical Communications*, 2008, 2206-2208.
- 216. X. Chen, S. Shen, L. Guo and S. S. Mao, *Chemical reviews*, 2010, **110**, 6503-6570.
- 217. A. Iwase, S. Yoshino, T. Takayama, Y. H. Ng, R. Amal and A. Kudo, *Journal of the American Chemical Society*, 2016, **138**, 10260-10264.
- 218. M. Woodhouse, G. Herman and B. Parkinson, *Chemistry of Materials*, 2005, **17**, 4318-4324.
- 219. S. Baeck, T. Jaramillo, C. Brändli and E. McFarland, *Journal of combinatorial chemistry*, 2002, 4, 563-568.
- 220. B. Parkinson, Energy & Environmental Science, 2010, 3, 509-511.
- 221. X. Chen, L. Liu, P. Y. Yu and S. S. Mao, Science, 2011, 331, 746-750.
- 222. K. Maeda and K. Domen, The Journal of Physical Chemistry Letters, 2010, 1, 2655-2661.
- D. Bokov, A. Turki Jalil, S. Chupradit, W. Suksatan, M. Javed Ansari, I. H. Shewael, G. H. Valiev and E. Kianfar, *Advances in Materials Science and Engineering*, 2021, 2021, 1-21.
- 224. T. J. Jacobsson, V. Fjällström, M. Sahlberg, M. Edoff and T. Edvinsson, *Energy & Environmental Science*, 2013, **6**, 3676-3683.
- 225. O. Khaselev, A. Bansal and J. Turner, *International Journal of Hydrogen Energy*, 2001, **26**, 127-132.
- 226. J. Brillet, J.-H. Yum, M. Cornuz, T. Hisatomi, R. Solarska, J. Augustynski, M. Graetzel and K. Sivula, *Nature Photonics*, 2012, **6**, 824-828.
- S. Y. Reece, J. A. Hamel, K. Sung, T. D. Jarvi, A. J. Esswein, J. J. Pijpers and D. G. Nocera, science, 2011, 334, 645-648.
- 228. F. F. Abdi, L. Han, A. H. Smets, M. Zeman, B. Dam and R. Van De Krol, *Nature communications*, 2013, 4, 2195.
- 229. F. H. Saadi, N. S. Lewis and E. W. McFarland, *Energy & environmental science*, 2018, 11, 469-475.

This article is licensed under a Creative Commons Attribution-NonCommercial 3.0 Unported Licence

Open Access Article. Published on 19 October 2023. Downloaded on 10/24/2023 3:00:04 PM

- 230. J. T. Hinkley, J. A. O'Brien, C. J. Fell and S.-E. Lindquist, *International journal of hydrogen energy*, 2011, **36**, 11596-11603.
- 231. A. Buttler and H. Spliethoff, *Renewable and Sustainable Energy Reviews*, 2018, **82**, 2440-2454.
- 232. A. T-Raissi and D. L. Block, *IEEE Power and Energy Magazine*, 2004, 2, 40-45.
- T. Nguyen, Z. Abdin, T. Holm and W. Mérida, Energy conversion and management, 2019,
 200, 112108.
- 234. C. C. Elam, C. E. G. Padró, G. Sandrock, A. Luzzi, P. Lindblad and E. F. Hagen, International Journal of Hydrogen Energy, 2003, 28, 601-607.
- 235. J. Romm, Energy policy, 2006, 34, 2609-2614.
- 236. R. Bhandari, C. A. Trudewind and P. Zapp, *Journal of cleaner production*, 2014, **85**, 151-163.
- 237. I. Sorrenti, Y. Zheng, A. Singlitico and S. You, *Renewable and Sustainable Energy Reviews*, 2023, **171**, 113033.
- 238. M. Z. Jacobson, W. Colella and D. Golden, Science, 2005, 308, 1901-1905.
- 239. C. Acar and I. Dincer, *International Journal of Global Warming*, 2017, **13**, 260-277.
- 240. C. Jørgensen and S. Ropenus, *International journal of hydrogen energy*, 2008, **33**, 5335-5344.
- 241. Ø. Ulleberg, T. Nakken and A. Ete, *International journal of hydrogen energy*, 2010, **35**, 1841-1852.
- 242. H. De Battista, R. J. Mantz and F. Garelli, Journal of Power Sources, 2006, 155, 478-486.
- 243. G. WEIDONG, International Journal of Hydrogen Energy, 2011.
- P. Denholm, G. L. Kulcinski and T. Holloway, *Environmental science & technology*, 2005,
 39, 1903-1911.
- 245. J. Sarkar and S. Bhattacharyya, Archives of thermodynamics, 2012, 33, 23-40.
- 246. J. Linnemann and R. Steinberger-Wilckens, *International Journal of Hydrogen Energy*, 2007, **32**, 1492-1499.
- 247. A. González, E. McKeogh and B. Gallachoir, Renewable energy, 2004, 29, 471-489.
- 248. R. Gazey, S. Salman and D. Aklil-D'Halluin, *Journal of Power Sources*, 2006, **157**, 841-847.
- 249. S. Shaw and E. Peteves, *International Journal of Hydrogen Energy*, 2008, **33**, 3249-3263.

- 250. T. J. Wallington, M. Grahn, J. E. Anderson, S. A. Mueller, M. Williander and K. Lindgren, Environmental science & technology, 2010, 44, 2702-2708.
- K. B. Martin and S. E. Grasman, *International journal of hydrogen energy*, 2009, 34, 6581-6588.
- 252. M. Granovskii, I. Dincer and M. A. Rosen, Journal of Power Sources, 2006, 157, 411-421.
- 253. M. Granovskii, I. Dincer and M. A. Rosen, *International Journal of Hydrogen Energy*, 2007, **32**, 927-931.
- 254. M. Aguado, E. Ayerbe, C. Azcárate, R. Blanco, R. Garde, F. Mallor and D. M. Rivas, International Journal of Hydrogen Energy, 2009, 34, 2845-2854.
- 255. K. Harrison, G. Martin, T. Ramsden, W. Kramer and F. Novachek, *Wind-to-Hydrogen Project: Operational Experience, Performance Testing, and Systems Integration*, National Renewable Energy Lab.(NREL), Golden, CO (United States), 2009.
- 256. T. Take, K. Tsurutani and M. Umeda, *Journal of Power Sources*, 2007, **164**, 9-16.
- 257. X.-W. Fang, L. Wang, W.-F. Cai, D.-W. Jing, Q.-Y. Chen and Y.-H. Wang, *international journal of hydrogen energy*, 2019, **44**, 15766-15770.
- 258. Z. Hu, M. Wu, Z. Wei, S. Song and P. K. Shen, *Journal of Power Sources*, 2007, **166**, 458-461.
- 259. E. Rasten, G. Hagen and R. Tunold, Electrochimica acta, 2003, 48, 3945-3952.
- D. L. Stojić, M. P. Marčeta, S. P. Sovilj and Š. S. Miljanić, *Journal of power sources*, 2003,
 118, 315-319.
- S. Grigor'ev, V. Porembskii and V. Fateev, *Chemical and Petroleum Engineering*, 2004, 40, 606-610.
- 262. H. Deligöz, S. Yılmaztürk, T. Karaca, H. Özdemir, S. N. Koc, F. Öksüzömer, A. Durmuş and M. A. Gürkaynak, *Journal of Membrane Science*, 2009, **326**, 643-649.
- 263. W. C. Choi, J. D. Kim and S. I. Woo, *Journal of Power Sources*, 2001, **96**, 411-414.
- 264. L. Jörissen, V. Gogel, J. Kerres and J. Garche, *Journal of Power Sources*, 2002, **105**, 267-273.
- X. Ma, J. Wang, D. Liu, R. Kong, S. Hao, G. Du, A. M. Asiri and X. Sun, New Journal of Chemistry, 2017, 41, 4754-4757.
- Z. Wang, L. Xu, F. Huang, L. Qu, J. Li, K. A. Owusu, Z. Liu, Z. Lin, B. Xiang and X. Liu, *Advanced Energy Materials*, 2019, 9, 1900390.

- 267. C. Wang, H. Lu, Z. Mao, C. Yan, G. Shen and X. Wang, *Advanced Functional Materials*, 2020, **30**, 2000556.
- 268. Y. Song, W. Xie, Y. Song, H. Li, S. Li, S. Jiang, J. Y. Lee and M. Shao, *Applied Catalysis B: Environmental*, 2022, **312**, 121400.
- Y. Wang, Y. Liu, D. Wiley, S. Zhao and Z. Tang, *Journal of Materials Chemistry A*, 2021,9, 18974-18993.
- 270. I. Dincer and C. Acar, *International Journal of Hydrogen Energy*, 2018, **43**, 8579-8599.
- 271. I. Dincer and C. Acar, *International journal of hydrogen energy*, 2015, **40**, 11094-11111.
- 272. F. Dawood, M. Anda and G. Shafiullah, *International Journal of Hydrogen Energy*, 2020, **45**, 3847-3869.
- 273. M. Ji and J. Wang, International Journal of Hydrogen Energy, 2021, 46, 38612-38635.
- 274. M. McPherson, N. Johnson and M. Strubegger, Applied Energy, 2018, 216, 649-661.
- 275. R. S. El-Emam and H. Özcan, Journal of Cleaner Production, 2019, 220, 593-609.
- 276. T. Sinigaglia, F. Lewiski, M. E. S. Martins and J. C. M. Siluk, *International journal of hydrogen energy*, 2017, **42**, 24597-24611.
- 277. A. Mehmeti, A. Angelis-Dimakis, G. Arampatzis, S. J. McPhail and S. Ulgiati, *Environments*, 2018, **5**, 24.
- 278. O. Siddiqui and I. Dincer, *International journal of hydrogen energy*, 2019, 44, 5773-5786.
- 279. C. Acar and I. Dincer, Journal of cleaner production, 2019, 218, 835-849.
- 280. R. E. Kopp and B. K. Mignone, *Economics*, 2012, **6**, 20120015.
- 281. F. C. Moore, U. Baldos, T. Hertel and D. Diaz, *Nature communications*, 2017, **8**, 1607.
- 282. Y. Cai and T. S. Lontzek, Journal of Political Economy, 2019, 127, 2684-2734.
- 283. R. S. Pindyck, Journal of Environmental Economics and Management, 2019, 94, 140-160.
- 284. M. Adler, D. Anthoff, V. Bosetti, G. Garner, K. Keller and N. Treich, *Nature Climate Change*, 2017, 7, 443-449.
- 285. M. A. DeLuchi, International Journal of Hydrogen Energy, 1989, 14, 81-130.
- 286. M. Momirlan and T. N. Veziroglu, *International journal of hydrogen energy*, 2005, **30**, 795-802.
- 287. M. Momirlan and T. Veziroglu, *Renewable and sustainable energy reviews*, 2002, **6**, 141-179.
- 288. J. Hord, International Journal of Hydrogen Energy, 1980, 5, 579-584.

- 289. L. Zhou, Renewable and Sustainable Energy Reviews, 2005, 9, 395-408.
- 290. H. J. Pasman and W. J. Rogers, *Journal of Loss Prevention in the Process Industries*, 2010, **23**, 697-704.
- 291. D. Das and T. N. Veziroglu, *International journal of hydrogen energy*, 2008, **33**, 6046-6057.
- 292. J. Zheng, X. Liu, P. Xu, P. Liu, Y. Zhao and J. Yang, *International journal of hydrogen energy*, 2012, **37**, 1048-1057.
- 293. A. Züttel, *Materials today*, 2003, **6**, 24-33.
- 294. B. Sakintuna, F. Lamari-Darkrim and M. Hirscher, *International journal of hydrogen energy*, 2007, **32**, 1121-1140.
- 295. G. Marbán Calzón and T. Valdés-Solís Iglesias, 2007.
- 296. J. Van Mierlo, G. Maggetto and P. Lataire, *Energy conversion and management*, 2006, **47**, 2748-2760.
- 297. I. Dincer and C. Acar, International Journal of Hydrogen Energy, 2017, 42, 14843-14864.
- 298. M. Fereidooni, A. Mostafaeipour, V. Kalantar and H. Goudarzi, *Renewable and Sustainable Energy Reviews*, 2018, **82**, 415-423.
- 299. C. Acar, A. Beskese and G. T. Temur, *International Journal of Hydrogen Energy*, 2018, 43, 18059-18076.
- 300. Y. Lim, C.-J. Lee, Y. S. Jeong, I. H. Song, C. J. Lee and C. Han, *Industrial & engineering chemistry research*, 2012, **51**, 4982-4989.
- 301. C. Acar and I. Dincer, Causes, impacts and solutions to global warming, 2013, 493-514.
- 302. U. N. Energy.
- 303. A. LE DUIGOU and P. ANZIEU, 2006.
- 304. T. Pregger, D. Graf, W. Krewitt, C. Sattler, M. Roeb and S. Möller, *International journal of hydrogen energy*, 2009, **34**, 4256-4267.
- 305. R. Elder and R. Allen, *Progress in Nuclear Energy*, 2009, **51**, 500-525.
- 306. E. Solomin, Z. Salah, K. Osintsev, S. Aliukov, S. Kuskarbekova, V. Konchakov, A. Olinichenko, A. Karelin and T. Tarasova, *Energies*, 2023, **16**, 6118.
- 307. R. S. El-Emam, H. Ozcan and I. Dincer, *International journal of hydrogen energy*, 2015, **40**, 11168-11177.
- 308. A. Godula-Jopek, Hydrogen production: by electrolysis, John Wiley & Sons, 2015.

- 309. M. Conte, F. Di Mario, A. Iacobazzi, A. Mattucci, A. Moreno and M. Ronchetti, *Energies*, 2009, **2**, 150-179.
- 310. C. Forsberg and M. Kazimi, 2010.
- 311. A. I. Osman, N. Mehta, A. M. Elgarahy, M. Hefny, A. Al-Hinai, A. a. H. Al-Muhtaseb and D. W. Rooney, *Environmental Chemistry Letters*, 2022, 1-36.

Corresponding Author's Profile:



Nisar Ahmed obtained his PhD in organic chemistry with Brain Korea BK21 fellowship from POSTECH, Korea. Then, he moved to the University of Zurich, Switzerland for a postdoctoral stay with an Innovative Novartis Fellowship. Subsequently, he joined the University of Bristol as a senior research associate. Further from 2017 he started his independent academic career at School of Chemistry, Cardiff University, United Kingdom. His fields of research include synthesis of value-added chemicals, fine chemicals, and pharmaceuticals with special focus on inert bonds activations & cleavage using modern synthetic tools such as electrochemistry, photochemistry, sonochemistry, flow technology, digital & automation chemistry, and reaction engineering.