

# Scrubbing process and chemical equilibria controlling the composition of light hydrocarbons in natural gas discharges: An example from the geothermal fields of El Salvador

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[1] The compositional features of fluids from both fumarolic discharges and productive geothermal wells of Ahuachapan-Chipilapa, Berlin-Chinameca, and San Vicente geothermal systems (El Salvador) are described and discussed in order to investigate the complex geochemical interactions involving geothermal fluids within the shallowest part of the hydrothermal circulation pathways. Our results highlight that secondary processes are able to strongly affect and modify the chemical characteristics of geothermal gases once they discharge to the surface as natural manifestations, mainly in relation to the chemical-physical properties of each gas species. The effects of both gas dissolution in shallow aquifers and gas-water-rock chemical interactions on gas discharge composition make it difficult to get a correct evaluation of the thermodynamic conditions that characterize the geothermal reservoirs by applying the common geoindicators based on the chemical equilibria of the H<sub>2</sub>O-CO<sub>2</sub>-H<sub>2</sub>-CH<sub>4</sub>-CO system. Differently, the composition of the C1-C2-C3 alkanes and the C3 and C4 alkane-alkene pair, established within the geothermal reservoirs under the control of chemical reactions, remains stable in samples collected from discharging gas vents. These results suggest that the relative abundances of hydrocarbons characterized by similar structure and molecular size seem to be mainly regulated by the diffusion velocity of gases through the liquid-dominated system. Therefore the chemical features of the light organic gas fraction of naturally discharging fluids can be successfully utilized for the evaluation of geothermal reservoir temperatures and redox conditions, providing useful indications in terms of geothermal exploration and exploitation. On this basis, the distribution, speciation, and relative abundances of light hydrocarbons can also be considered highly promising in geochemical monitoring of active volcanic systems.



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### 1. Introduction

[2] The chemical composition of natural gas discharges in volcanic and hydrothermal systems is controlled by complex physical-chemical processes [e.g., Giggenbach, 1997]. In this respect, interactions between circulating thermal fluids and shallow environment, as well as inputs from external sources (e.g., radiogenic elements, air and bacterial activity) and boiling and steam condensation processes [e.g., Giggenbach, 1980; Giggenbach et al., 1986; Chiodini and Marini, 1998], often play a fundamental role. Several geochemists [e.g., Ellis and Mahon, 1977; Armannson et al., 1982; Hedenquist and Lowenstern, 1994] agree that hydrothermal systems are able to completely dissolve magmaticrelated gas compounds producing acidic fluids and promoting strong hydrothermal alteration, which is at the base of the mineral/ore forming processes. Generally speaking, gas scrubbing can be regarded as any secondary physical-chemical process, comprehending dissolution into the aqueous phase and formation of precipitates (e.g., sulfur, sulfides, fluorides, sulfates) from either gas-water or gaswater-rock reactions, able to modify, at least partially, the composition of the gas species in thermal fluids [e.g., Symonds et al., 1994, 2001]. The effects of this phenomenon were first recognized by Doukas and Gerlach [1995] to explain low SO<sub>2</sub> emissions before and between the 1992 eruption of Crater Peak at Mount Spurr. Reaction path modeling has been used to describe magmatic gas scrubbing taking place during interactions of magmatic gas with air-saturated water and rock [Symonds et al., 2001; Marini and Gambardella, 2005].

[3] Whatever the conceptual model adopted, these studies have stressed the importance that the influence of secondary interactions can assume for the chemical features of natural discharging fluids, especially those related to hydrothermal systems. This suggests that, when the chemical and isotopic features of fluid discharges are used to investigate thermochemical conditions governing the deep reservoirs, the influence of secondary processes has to be severely evaluated. Geothermometers based on equilibrium reactions involving gas species, e.g., CO<sub>2</sub>-CH<sub>4</sub>-H<sub>2</sub>-H<sub>2</sub>S [D'Amore and Panichi, 1980; Arnosson and Gunnlaugsson, 1985], CO<sub>2</sub>-CH<sub>4</sub> [Giggenbach, 1996; Taran, 1986], CO<sub>2</sub>-CO [Chiodini et al., 2001] and H<sub>2</sub>-Ar [Giggenbach, 1991], commonly adopted to calculate reservoir temperatures in geothermal areas, are able to provide reliable results especially when gases from deep wells, like those used for the exploitation of geothermal energy that allow a rapid up-flow of fluids toward the surface without significant interactions with the surrounding environment, are considered. Nevertheless, in active volcanoes and hydrothermal systems these artificial gas conduits are rarely present. This can represent a serious limitation for both geochemical investigations of geothermal resources [e.g., D'Amore and Nuti, 1977; Bertrami et al., 1985; Arnorsson, 1990; D'Amore, 1991] and geochemical monitoring of active volcanoes [e.g., Menyailov, 1975; Giggenbach, 1987; Marini et al., 1991; Chiodini et al., 1993].

[4] In a geothermal area the compositional differences between fluids from wells and natural gas vents, which have the same source but characterized by different fluid pathways, are likely to be mainly related to the physical-chemical processes that may occur in the shallower part of the fumarolic conduits. As a consequence, the comparison between well and fumarolic gas chemistry has to be considered particularly useful to understand the effects that the shallow processes may have as deep fluids rise from the source area to the surface. According to these considerations, the main goal of this study, based on the chemical data of the gas



**Figure 1.** Schematic maps of (a) El Salvador, (b) Ahuachapan-Chipilapa geothermal field, (c) Berlin geothermal field, and (d) San Vicente volcano. The location of the gas sampling sites is also reported.

samples collected from both geothermal wells and fumaroles from Ahuachapan-Chipilapa, Berlin, Chinameca and San Vicente geothermal fields (El Salvador) (Figure 1), is to evaluate the effects of secondary processes on the chemical composition of naturally discharging gases in hydrothermal environment. A particular attention is devoted to verify the usefulness of light hydrocarbons as possible geo-indicators for volcanic and geothermal systems [e.g., *Tassi et al.*, 2005a, 2005b], since this group of gas species has similar chemical-physical features and, consequently, they are supposed to show similar behavior in response to secondary processes.

### 2. General Features of the Geothermal Systems of El Salvador

# 2.1. Geothermal Energy Exploitation Activity

[5] The exploration of geothermal resources in El Salvador commenced in 1954 and is still on, although it was suspended because of the 1980–1992 civil war [*Huttrer*, 2001]. Within the framework of this activity, ten geothermal areas,

characterized by medium-to-high temperature (180-300°C) fluids, have been identified [Monterrosa, 1998]. Geothermal energy production in the Ahuachapan-Chipilapa geothermal field, located approximately 80 km west of San Salvador, started in 1975. Forty wells have been drilled (590 to 1524 m deep) in an area of approximately 5 km<sup>2</sup>, but presently only 8 wells, able to produce up to 63 MW, are in continuous operation [Jacobo, 2003]. Geothermal exploration at the Berlin field started in 1976 [Cuellar, 1981] and developed in 1978-1981, when five wells were drilled. Since 1992, when two 5 MW backpressure power units were installed, the Berlin geothermal field has continuously been exploited. From 1997 to 1999, 18 wells (8 producers and 10 injectors), at depth between 1500 and 2400 m, were drilled and a power plant was constructed, for a total geothermal capacity of 56 MW. After 2000, four wells were drilled in the southern part of the geothermal field in order to assess the possibility of installing a third power unit of 28 MW [Renderos, 2002]. Presently, the geothermal plants installed in El Salvador are able to produce about 161 MW (95 MW from Ahuachapan-Chipilapa and 66 MW from Berlin), accounting for the 24% of the country electricity output [*Rodriguez and Herrera*, 2003]. San Vicente geothermal system, close to the homonymous volcano (Figure 1a), has been discovered only in the late 1970s, with the drilling of an exploration well and few shallow boreholes. Further geophysical (gravimetric and geoelectric) investigations have allowed to estimate an energy production of about 50 MW [*Huttrer*, 2001].

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# 2.2. Geology Overview and Chemistry of the Geothermal Fluids

[6] El Salvador is a seismologically active region of the southern-east coast of Central America, where the Cocos plate is subducting under the Caribbean plate at rates of 92 mm/yr along the Middle America Trench that is located 100 km offshore [Schmidt-Thomé, 1975; Weber, 1978; Bourgois et al., 1984]. Parallel to this trench runs the Central American graben, a 20-km-wide E-W oriented tectonic depression that in the southern part borders a Quaternary volcanic chain (Figure 1a), whose magmas likely represent the heat source of the widespread geothermal activity in the region. The location of the four distinct geothermal areas (Auhachapan-Chipilapa, Berlin, Chinameca and San Vicente) the present study is referred to, is reported in Figures 1a–1d.

[7] The Ahuachapan-Chipilapa geothermal field (Figure 1b) is located in western El Salvador between the Santa Ana volcanic complex and the Guatemala border (Figure 1a). It lies within the 6-km-wide Pleistocene caldera of Concepcion de Ataco that is part of the Apaneca volcanic complex (also known as the Cuyanausol Range) consisting of roughly E-W oriented Pleistocene and Holocene stratovolcanoes. The post-caldera cones of Cerro El Aguila (2036 m a.s.l., the highest peak of the complex) and Cerro Los Naranjos volcanoes, at the eastern end of the Apaneca Range, and the young craters of Laguna Verde stratovolcano may have been active during the Holocene [Gonzales Partida et al., 1997]. The volcanic sequence of the Concepcion de Ataco caldera, whose volume approaches about 63 km<sup>3</sup> [Gonzales Partida et al., 1997], is composed by basaltic andesites to dacitic-ryolitic [Aumento et al., 1982] alternated layers of tuff, lava and pyroclastic sequences [Montalvo, 1994]. The tectonic structure is controlled by E-W, associated to the Central American graben, and NE-SW trending fault systems. The geothermal field, which is characterized by numerous hot springs, bubbling pools and fumaroles [Gonzales Partida et al., 1997], is the largest one under exploitation in El Salvador. Its heat source seems to be related to the presence of an andesitebasalt magmatic chamber (0.1 Ma) located at the depth of 9 km [Jacobo, 2003]. Geophysical measurements suggest that Ahuachapan and Chipilapa can be regarded as two distinct hydrothermal systems [Romo et al., 1997], separated by a hydrological barrier resulting by an uplift structure [Gonzales Partida et al., 1997]. Nevertheless, the chemical and isotopic features of the geothermal fluids of the two areas seem to indicate the existence of a common deep reservoir. When the exploitation activity commenced, fluids were characterized by a temperature of about 230-260°C with chloride contents up to 9000 mg/L [D'Amore and Mejia, 1999]. As the geothermal exploitation proceeded the chemical features of the main reservoir significantly changed, as testified by the compositional evolution of the geothermal wells that suffered (1) a decrease of the Cl contents down to about 6000 mg/L, (2) an increase of SO<sub>4</sub> contents, and (3) an increase of CO<sub>2</sub>, H<sub>2</sub>S and H<sub>2</sub> partial pressures [Truesdell et al., 1989; Nieva et al., 1997; Jacobo, 2003].

[8] The Berlin geothermal field (Figure 1c), located 100 km east of San Salvador at an elevation between 600 and 900 m a.s.l., is associated to the Pleistocene Tecapa-Berlin volcanic complex that consists of a series of peripheral volcanic cones emerging around the Berlin caldera. The latter formed after the final activity (0.1 Ma) of the old Berlin volcano, which is characterized by basaltic to andesitic lava flows and scoria and andesitic to dacitic ignimbrites [Jacobo, 2003], and is marked by a NE-SW oriented fault system and a NNW-SSE transverse fault, along which several hot fluid discharges are aligned. Geophysical investigations suggest that the heat source of the Berlin geothermal field is a recent andesite magma chamber that lies at a depth of about 6 km, south of the present geothermal field where the most recent volcanic edifices (El Hoyon and Cerro de Alegria; Figure 1c) are located [D'Amore and Mejia, 1999]. At Berlin, the chemical-physical conditions of the reservoir are quite different with respect to those of the Ahuachapan-Chipilapa field. The maximum temperature measured in the geothermal wells, that reach a depth of 2300 m, was up to 305°C [Montalvo and Axelsson, 2000]; Cl contents, when the exploitation activity started, were up to 11,000 mg/L [D'Amore and Mejia, 1999]. Furthermore, reinjection has been adopted since the beginning of the geothermal energy production, while at Ahuachapan-Chipilapa no fluid reinjection



has presently been performed. Reinjected fluids strongly affected both the chemical and the isotopic parameters of the Berlin geothermal reservoir. Chloride contents progressively lowered down to about 3000-7000 mg/L [Montalvo and Axelsson, 2000; Jacobo, 2003], while the  $\delta^{18}$ O and  $\delta$ D isotopic ratios were intermediate between those of the local recharge meteoric water and the reinjected water [Renderos, 2002].

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[9] Chinameca, a relatively small geothermal area located few tens of km east of the Berlin caldera (Figure 1a), is marked by the presence of fumaroles, locally named "Infernillos de Chinameca," suggesting the presence of hot fluids at depth, but no geothermal exploration have been carried out and little is known about its geological and structural settings. In the present study we will be referring to the Berlin-Chinameca geothermal field as a unique system, although the two areas are likely characterized by distinct hydrothermal reservoirs.

[10] San Vicente is a Quaternary stratovolcano (2183 m a.s.l.) (Figure 1d), located in the central region of El Salvador (Figure 1a), which rises inside the Pliocene Central American graben. Its activity started in the Tertiary with mild and episodic emissions of tholeitic lavas. In the Pleistocene several paroxistic events took place, leading to the collapse of the old edifice, known as La Carbonera, and giving rise to the formation of the caldera structure [Barberi et al., 1995]. The modern San Vicente volcano grew during the Holocene within the caldera. Its edifice consists of two prominent cones that are largely composed of andesite lava flows. On the basis of their morphology, the easternmost cone appears to be the youngest, suggesting that the focus of volcanism has migrated east-northeastward with time. No historical eruptions have been recorded from this apparatus, although volcano-related events, like lahars, have occurred several times (e.g., in 1774, 1934, 1996 and 2001) [Major et al., 2001]. A preliminary investigation carried out by the Salvadorian State Agency for Electric Power indicated a relatively high geothermal gradient  $(0.2^{\circ}C/m)$ , suggesting the presence of a hydrothermal reservoir at a depth ranging between 1100 and 1300 m, characterized by a temperature of about 250°C, consistent with that estimated on the basis of the chemistry of the fumarolic fluids [Aiuppa et al., 1997]. Presently, a moderate fumarolic activity, whose physical-chemical features are almost identical to those of the fumaroles seeping out at Ahuachapan-Chipilapa and Berlin-Chinameca geothermal fields, is present in two areas (Agua Agria and Infernillos Ciegos, respectively) along the northern and western flanks of the volcano (Figure 1d) [*Aiuppa et al.*, 1997].

## 3. Sampling and Analytical Methods

[11] Gas samples were collected during two sampling campaigns carried out in February and April 2004 at (1) Ahuachapan-Chipilapa (8 fumaroles and 7 geothermal wells), (2) Berlin-Chinameca (6 fumaroles and 2 geothermal wells), and (3) San Vicente (4 fumaroles) geothermal areas (Figures 1a-1d). Gas samples from the geothermal wells were collected as separated steam from an industrial separator where gas pressure was about 7 bars. Gases were stored into pre-weighted and preevacuated 50-mL Thorion-tapped pyrex tubes, containing 20 mL of a 0.15M Cd(OH)<sub>2</sub> and 4M NaOH suspension. Acidic gases (CO<sub>2</sub>, HF and HCl) and water vapor were dissolved into the alkaline solution, H<sub>2</sub>S reacted with Cd<sup>2+</sup> and precipitated as CdS, while residual gases were collected in the headspace. Separate aliquots of condensate were devoted to the analysis of Cl and F. Inorganic gas compounds were analyzed by acidimetric titration (CO<sub>2</sub>), ion chromatography (Cl, F, SO<sub>2</sub>, H<sub>2</sub>S) and gas chromatography (N2, O2, CO, H2, He, Ar and Ne), following the procedure described by Montegrossi et al. [2001]. To obtain a satisfactory separation of H<sub>2</sub>, He and Ne peaks a 10 m long molecular sieve column, at the temperature of  $0^{\circ}$ C and using Ar as gas carrier, was utilized. The organic gas fraction (CH<sub>4</sub>, C<sub>2</sub>-C<sub>9</sub> hydrocarbons, C<sub>4</sub>H<sub>4</sub>O, C<sub>4</sub>H<sub>4</sub>S, C<sub>5</sub>H<sub>6</sub>O, C<sub>5</sub>H<sub>6</sub>S and (CH<sub>3</sub>)<sub>2</sub>S) was analyzed by gas chromatography. The complete separation of the peaks of the 30 different organic gas compounds was performed by using 2 different chromatographic columns: (1) a 10 m long stainless steel column (N = 2 mm) packed with Chromosorb PAW 80/100 mesh coated with 23% SP 1700, for the determination of C1-C5 hydrocarbons, and (2) a 2.5 m long stainless steel column (N = 2 mm) packed with Chromosorb PAW 100/120 mesh coated with 10% TCEP, for the determination of C<sub>6</sub>-C<sub>9</sub> hydrocarbons [Tassi et al., 2004].

[12] Analytical precision is <5% for major gas components and <10% for minor and trace compounds.

#### 4. Results

# 4.1. Gas Temperature and Composition of the Inorganic Gas Fraction

[13] The outlet temperatures, the H<sub>2</sub>O contents and the composition of the inorganic gases (dry gas

**Table 1.** Chemical Composition of the Dry Gas Fraction (Inorganic Gases) and Outlet Temperatures of the Fumaroles and the Geothermal Wells From the Ahuachapan-Chipilapa, Berlin-Chinameca, and San Vicente Geothermal Fields<sup>a</sup>

	Name	Location	T, ℃	$CO_2$	$H_2S$	$N_2$	Ar	O <sub>2</sub>	Ne	$H_2$	He	СО	H <sub>2</sub> O
1	El Playon	Ahuachapan	99.4	828,965	1,266	157,977	852.8	992.1	0.561	9,988	4.196	1.189	992,930
2	Chipilapa	Ahuachapan	99.7	948,492	2,954	46,294	92.18	1,463	0.056	698.6	8.170	1.216	996,116
3	Agua caliente M2	Ahuachapan	99.2	952,606	31,180	15,587	160.8	7.184	0.096	486.4	5.044	< 0.001	988,168
4	Zapote	Ahuachapan	101.7	893,874	4,608	91,500	620.4	6,563	0.406	2,799	18.36	1.117	995,991
5	Termopilas hervideros	Ahuachapan	94.7	932,148	2,551	59,118	670.3	1,199	0.432	4,324	10.52	1.831	993,760
6	Termopilas fumarola	Ahuachapan	100.5	943,767	4,610	47,607	367.2	59.31	0.237	3,454	9.324	1.960	995,987
7	El Tortuguero hervideros	Ahuachapan	93.0	951,050	10,320	35,114	118.4	1,444	0.066	1,912	4.725	1.745	988,377
8	Tortuguero Fumarola	Ahuachapan	98.9	964,609	5,868	25,935	92.29	1,154	0.050	2,352	2.792	1.568	995,617
9	Tronador	Berlin	99.4	952,288	10,394	34,780	215.1	206.5	0.135	2,169	5.658	1.536	997,917
10	TR6	Berlin	98.0	950,342	7,810	35,210	427.8	3,940	0.281	2,345	1.148	0.838	997,600
11	Laguna Alegria	Berlin	98.5	947,452	36,090	12,821	32.76	285.7	0.024	3,310	8.227	1.570	975,351
12	Oyon Crater	Berlin	97.7	955,221	31,323	8,290	28.11	52.45	0.022	5,070	2.266	2.676	976,027
13	Infernillos Cinameca	Cinameca	98.0	935,358	13,938	48,797	335.2	207.3	0.229	1,491	1.294	1.324	998,353
	hervideros												
14	Infernillos Cinameca Fumarola	Cinameca	99.4	759,627	2,400	229,598	1621	818.9	1.071	5,980	6.094	1.428	997,786
15	Infermillos Ciegos	San Vicente	92.0	970,656	11,973	13,606	213.7	1,068	0.132	2,464	1.519	0.792	993,572
	Hervideros												
16	Infernillos Ciegos Fumarole	San Vicente	101.7	936,944	9,587	43,708	535.0	2,472	0.336	6,802	4.629	1.897	997,345
17	Agua Agria	San Vicente	92.0	950,054	9,063	35,302	290.8	3,039	0.188	2,246	6.261	1.390	986,917
	hervideros												
18	Agua Agria Fumarole	San Vicente	100.0	960,139	5,335	30,162	153.7	65.64	0.100	4,173	5.583	1.520	996,885
19	AH 6	Ahuachapan	150	949,868	18,866	27,934	176.4	< 0.001	n.d.	3,199	2.051	3.691	997,817
20	AH 16A	Ahuachapan	150	960,005	16,519	22,695	216.2	27.03	n.d.	573.0	< 0.001	1.535	996,297
21	AH 17	Ahuachapan	150	983,283	7,709	8,693	75.86	< 0.001	n.d.	332.1	2.936	2.235	995,057
22	AH 20	Ahuachapan	150	979,935	13,027	6,482	34.70	< 0.001	n.d.	492.2	< 0.001	1.574	995,922
23	AH 23	Ahuachapan	150	971,160	3,912	24,320	68.79	< 0.001	n.d.	501.7	7.823	1.446	995,885
24	AH 31	Ahuachapan	150	982,287	8,722	8,426	93.20	< 0.001	n.d.	441.6	2.031	2.491	995,664
25	AH 35	Ahuachapan	150	966,018	15,030	18,330	132.9	8.638	n.d.	352.5	5.842	0.947	996,527
26	Berlin 5V	Berlin	180	971,785	11,926	14,810	112.4	< 0.001	n.d.	1,481	< 0.001	0.864	997,017
27	Berlin 5C	Berlin	180	982,343	9,429	7,430	58.73	< 0.001	n.d.	811.9	2.514	0.774	996,778

<sup>a</sup>Outlet temperatures are in °C. Gas contents are in  $\mu$ mol/mol.

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fraction) of the fumarolic discharges and the geothermal wells from the three El Salvador geothermal fields are reported in Table 1.

[14] The fumarolic outlet temperatures range in a narrow interval (between 92 and 101.7°C) close to the temperature of boiling water at atmospheric pressure, while the temperatures of the Ahuachapan-Chipilapa and Berlin-Chinameca geothermal wells, measured at the outlet of the water-steam separator, were about 150 and 180°C, respectively, which are significantly lower than those measured at well bottoms [*D'Amore and Mejia*, 1999] likely due to steam-liquid separation process.

[15] H<sub>2</sub>O is largely the dominant component (up to 998,377  $\mu$ mol/mol) in both the fumaroles and the geothermal wells, whereas the dry gas fraction is

mainly represented by CO2 (between 759,627 and 983,283  $\mu$ mol/mol) and H<sub>2</sub>S (up to 36,090  $\mu$ mol/ mol), as typically occurs for geothermal fluids [e.g., Giggenbach, 1980, 1991]. Among the residual gases, N<sub>2</sub> (up to 229,598  $\mu$ mol/mol) and H<sub>2</sub> (up to 9,988 µmol/mol) are the most abundant compounds, O<sub>2</sub> and Ar contents show large variations (between <0.001 and 6,563 and 28.11 and 1,621  $\mu$ mol/mol, respectively), while only minor contents of He (up to 18.36  $\mu$ mol/mol) and CO (up to 3.691  $\mu$ mol/mol) were measured. The relatively low Ne contents (1.071  $\mu$ mol/mol) seem to exclude any significant air-contamination during the gas sampling. The composition of our geothermal gases from both Ahuachapan-Chipilapa and Berlin-Chinameca geothermal fields is consistent

with those reported by *Renderos* [2002] and *Jacobo* [2003].

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### 4.2. Origin of Steam and Inorganic Gases

[16] The geothermal reservoirs is mainly recharged by meteoric water, although, the  $\delta^{18}$ O and  $\delta$ D values of steam from the geothermal wells [e.g., Nieva et al., 1997; Montalvo and Axelsson, 2000; Renderos, 2002] suggest that a significant contribution of andesitic water [Taran et al., 1989; Giggenbach, 1992] cannot be ruled out [D'Amore and Mejia, 1999]. The presence of a deep component is also supported by the carbon ( $\delta^{13}$ C in CO<sub>2</sub>) and helium isotopic composition, whose values are between -1.5 and -2.8 % PDB-V [Snyder et al., 2001, 2003] and 5 and 7 (as R/R<sub>air</sub>) [Snyder et al., 2001], respectively. The  $N_2/Ar$  ratios are generally higher (up to 502) than that of the air (83.6), consistent with those reported by D'Amore and Mejia [1999] and Jacobo [2003], and suggest a considerable contribution of non-atmospheric N<sub>2</sub>, as commonly observed in fluids discharging in areas located along convergent plate boundaries [Giggenbach, 1996]. Differently, the Ar/Ne ratios, approaching those of ASW (Air Saturated Water: 1,700 to 940 for pure water at temperature ranging from 20 to 80°C), indicate that the atmosphericrelated compounds are added to the hydrothermal systems as dissolved phases in the meteoricoriginated water recharging the geothermal reservoirs. The  $O_2/Ar$  ratios (between 0 and 15.87) are significantly lower than that of ASW ( $\approx 20$ ), and this is likely related to O<sub>2</sub>-consumption by redox reactions among gas species and during water-rock interaction.

# 4.3. Composition of the Organic Gas Fraction

[17] The organic fraction composition (dry gas fraction) of fumarolic and geothermal well discharges is reported in Table 2.

[18] Up to 25 different hydrocarbons were detected and quantified. Among the alkanes, methane is the most abundant compound (between 7.64 and 839.5  $\mu$ mol/mol), while ethane (up to 68.47  $\mu$ mol/ mol), propane (up to 86.94  $\mu$ mol/mol) and the C<sub>4</sub>-C<sub>9</sub> normal- and iso-alkanes progressively decrease as the molecular size increases. A similar behavior is also shown by the relative abundances of benzene (up to 9.135  $\mu$ mol/mol), toluene (up to 2.06  $\mu$ mol/mol), xylene (the sum of its meta- and para-isomers; up to 0.452  $\mu$ mol/mol) and ethylbenzene (up to 0.329  $\mu$ mol/mol), all pertaining to the aromatics group. Iso-butene and propene are by far the most abundant alkenes (up to 23.13 and 9.257  $\mu$ mol/mol, respectively), while traces of trans-2-butene and cis-2-butene were detected only in few cases (Table 2). Besides the C-H species, five further organic gas compounds, dimethylsulfide, thiophene, methyl-thiophene, furane and methyl-furane, were detected in some gas samples, although in very low amounts ( $\leq 0.068 \mu$ mol/mol; Table 2).

# 4.4. Origin of the Organic Gases

[19] The presence of many different organic gas compounds, which is consistent with the compositional characteristics observed in other hydrothermal systems [e.g., Capaccioni et al., 1993, 2004; Tassi, 2004; Tassi et al., 2005a, 2005b], can be regarded as a peculiar feature for geothermal fluids. Organic matter ("kerogen") is likely the main hydrocarbon source [e.g., Gunter, 1978; Des Marais et al., 1981; Mango, 2000], since abiotic synthesis from inorganic constituents contributing to hydrocarbon production at hydrothermal conditions, though possible [e.g., Berndt et al., 1996; Horita and Berndt, 1999], can be regarded as negligible [e.g., Welhan, 1988; Darling, 1998; Mango, 2000; Taran and Giggenbach, 2003]. The ratio between CH<sub>4</sub> and light hydrocarbons can provide some useful information on the temperature conditions characterizing the genetic process of these compounds. The  $CH_4/(C_2H_6 + C_3H_8)$  ratio ranges between 2 and 108 and indicates that the hydrocarbons are thermogenically produced (T >  $150^{\circ}$ C) [e.g., Oremland et al., 1987; Whiticar and Suess, 1990]. This implies that (1) the organic matter evolved at depth, possibly within the geothermal reservoirs, and (2) no significant contribution by bacterial activity, which typically occurs in shallow environments at T < 50°C generating almost pure CH<sub>4</sub> [Hunt, 1984], was added to the geothermal fluids.

[20] The previously mentioned presence of sulfursubstituted hydrocarbons in some of our gas samples can be considered a common feature for natural gases [e.g., *Mangani et al.*, 2004], these compounds being easily produced in presence of  $H_2S$  even at low-to-medium temperatures. Differently, the two relatively unstable oxygen-substituted heterocyclic, furane and methyl-furane, that were detected only in two fumaroles of the Berlin-Chinameca geothermal field (Laguna Alegria and Oyon Crater gas samples; Table 2), are rarely found in geothermal gases being typical of fuma-

Chi	nameca, and San Vicente Ueot	nermal Fields												
	Name	Location	$CH_4$	$C_2H_6$	$\rm C_3H_8$	$C_3H_6$	$i\text{-}C_4H_{10}$	$n-C_4H_{10}$	$i-C_4H_8$	$t-2-C_4H_8$	$c-2-C_4H_8$	$i\text{-}C_5H_{12}$	$n-C_5H_{12}$	$2.3$ -dimetil- $C_4H_{10}$
-	El Playon	Ahuachapan	147.1	12.04	6.070	0.369	0.432	1.478	1.104	<0.0001	< 0.0001	0.1189	0.4271	0.1911
2	Chipilapa	Ahuachapan	40.67	1.696	0.470	0.019	0.140	0.153	0.219	< 0.0001	< 0.0001	0.0023	0.0314	0.0023
3	Agua caliente M2	Ahuachapan	86.39	2.284	0.387	0.019	0.115	0.060	0.058	< 0.0001	< 0.0001	0.0035	0.0098	0.0014
4	Zapote	Ahuachapan	51.07	1.823	0.438	0.023	0.406	0.191	0.394	< 0.0001	< 0.0001	0.0196	0.0208	0.0113
2	Termopilas hervideros	Ahuachapan	89.66	1.624	0.206	0.015	0.035	0.034	0.111	< 0.0001	< 0.0001	0.0243	0.0545	0.0101
9	Termopilas fumarola	Ahuachapan	82.10	1.490	0.186	0.013	0.027	0.047	0.077	0.0206	< 0.0001	0.0191	0.0236	0.0061
7	El Tortuguero hervideros	Ahuachapan	56.14	0.981	0.116	0.008	0.057	0.019	0.033	<0.0001	< 0.0001	0.0019	0.0062	0.0047
8	Tortuguero Fumarola	Ahuachapan	38.66	0.645	0.074	0.005	0.010	0.013	0.036	< 0.0001	< 0.0001	0.0075	0.0167	0.0062
6	Tronador	Berlin	99.03	0.979	0.063	0.005	0.019	0.068	0.064	< 0.0001	< 0.0001	0.0190	0.0283	0.0357
10	TR6	Berlin	78.30	2.384	0.435	0.032	1.502	0.303	0.771	0.0587	0.0209	0.0203	0.0132	0.0061
11	Laguna Alegria	Berlin	144.0	1.256	0.066	0.025	0.005	0.006	0.015	<0.0001	< 0.0001	0.0061	0.0229	0.0100
12	Oyon Crater	Berlin	7.639	0.174	0.025	0.011	0.002	0.002	0.007	0.0013	< 0.0001	0.0009	0.0015	0.0009
13	Infernillos Cinameca hervideros	Cinameca	109.5	5.977	2.286	0.100	0.199	0.563	0.487	0.0116	< 0.0001	0.0858	0.1571	0.0160
14	Infernillos Cinameca Fumarola	Cinameca	304.7	18.87	8.047	0.379	0.743	0.167	0.282	<0.0001	< 0.0001	0.0340	0.0433	0.0202
15	Infermillos Ciegos Hervideros	San Vicente	293.8	4.581	0.499	0.025	0.037	0.054	0.070	0.0264	< 0.0001	0.0064	0.0124	0.0172
16	Infernillos Ciegos Fumarole	San Vicente	839.5	13.165	1.440	0.077	0.102	0.169	0.199	<0.0001	< 0.0001	0.0138	0.0355	0.0313
17	Agua Agria hervideros	San Vicente	45.19	0.859	0.111	0.005	0.039	0.018	0.015	<0.0001	< 0.0001	0.0035	0.0058	0.0018
18	Agua Agria Fumarole	San Vicente	123.4	2.434	0.324	0.015	0.022	0.045	0.047	<0.0001	< 0.0001	0.0009	0.0056	< 0.0001
19	AH 6	Ahuachapan	217.4	43.83	56.60	5.083	7.208	11.743	9.973	0.0216	0.0070	1.5721	2.5428	0.1039
20	AH 16A	Ahuachapan	379.7	68.47	86.94	9.257	7.031	18.047	23.13	< 0.0001	< 0.0001	2.5973	4.4334	0.0446
21	AH 17	Ahuachapan	56.18	5.213	3.272	0.317	0.395	0.767	0.731	<0.0001	< 0.0001	0.0351	0.0525	0.0093
22	AH 20	Ahuachapan	57.08	5.379	3.419	0.350	1.808	1.467	1.921	<0.0001	< 0.0001	0.2404	0.3339	0.0159
23	AH 23	Ahuachapan	187.9	28.06	25.935	2.126	1.661	6.973	2.417	< 0.0001	< 0.0001	1.5306	1.6752	0.0850
24	AH 31	Ahuachapan	14.84	1.244	0.621	0.059	0.180	3.762	0.689	<0.0001	< 0.0001	0.0320	0.0498	0.0061
25	AH 35	Ahuachapan	88.63	7.526	4.155	0.360	1.722	4.532	0.949	<0.0001	< 0.0001	0.0590	0.1521	0.0109
26	Berlin 5V	Berlin	151.5	9.789	3.951	0.319	1.373	0.999	2.828	< 0.0001	< 0.0001	0.1099	0.2541	0.0094
27	Berlin 5C	Berlin	113.7	4.094	0.950	0.111	0.527	1.769	1.691	0.0035	<0.0001	0.0434	0.0925	0.0034
а (	as contents are in umol/mol.													



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	Molecular Volume	(mean well)	Std. Dev. Wells	(mean fum)	Std. Dev. Fumaroles	(mean fum)/(mean well)
H <sub>2</sub> S	43.4	11,624	4,723	11,129	10,630	0.96
$\overline{CO_2}$	42.9	966,572	11,396	924,319	53,074	0.96
N <sub>2</sub>	38.7	15,389	8,190	53,736	55,852	3.49
Ar	32.0	107.1	58.24	377.9	389.0	3.53
H <sub>2</sub>	26.5	906	927.3	3432	2349	3.79
He	23.8	2.565	2.700	5.847	4.140	2.28
CO	39.5	1.720	0.940	1.414	0.560	0.82
$CH_4$	42.1	140.4	111.4	145.7	190.2	1.04
$C_2H_6$	65.1	19.26	23.00	4.058	5.220	0.21
$C_3H_8$	90.5	20.63	30.92	1.178	2.230	0.06
$n-C_4H_{10}$	116.4	5.545	5.870	0.188	0.350	0.03
$n-C_5H_{12}$	144.9	1.144	1.520	0.051	0.100	0.04
$n-C_6H_{14}$	174.4	0.622	0.540	0.044	0.050	0.07
$n-C_7H_{16}$	204.9	0.125	0.152	0.009	0.014	0.07
n-C <sub>8</sub> H <sub>18</sub>	237.4	0.069	0.068	0.006	0.009	0.08
n-C9H20	271.2	0.026	0.027	0.002	0.004	0.09
$i-C_4H_{10}$	114.9	2.429	2.720	0.216	0.376	0.09
$i-C_5H_{12}$	141.3	0.727	0.948	0.021	0.031	0.03
i-C <sub>6</sub> H <sub>14</sub>	170.2	0.257	0.178	0.011	0.020	0.03
i-C <sub>7</sub> H <sub>16</sub>	200.7	0.178	0.135	0.002	0.004	0.01
i-C <sub>8</sub> H <sub>18</sub>	232.3	0.169	0.145	0.002	0.003	0.01
i-C <sub>9</sub> H <sub>20</sub>	240.8	0.066	0.048	0.001	0.002	0.01
$C_6H_6$	119.3	3.171	2.760	1.609	1.490	0.51
$C_7H_8$	149.7	0.534	0.623	0.063	0.050	0.12
m-p-C <sub>8</sub> H <sub>10</sub>	178.5	0.130	0.133	0.011	0.010	0.09
$C_3H_6$	82.4	1.996	3.170	0.063	0.116	0.03
$i-C_4H_8$	101.9	4.917	7.400	0.221	0.299	0.04

**Table 3.** Mean Contents, Standard Deviations, and Molecular Volumes of the Fumaroles and the Geothermal Wells From the Ahuachapan-Chipilapa, Berlin-Chinameca, and San Vicente Geothermal Fields for Selected Gas Species<sup>a</sup>

<sup>a</sup>Mean contents are in  $\mu$ mol/mol, standard deviations are in  $\mu$ mol/mol, and molecular volumes are in cm<sup>3</sup>/mol. Definitions: (*mean fum*), fumaroles; (*mean well*), geothermal wells. Mean contents were calculated on the basis of the composition of the dry gases. The (*mean fum*)/(*mean well*) ratios were also reported.

rolic emissions in active volcanic systems [Tassi, 2004; Capaccioni et al., 2005].

### 5. Effects of Scrubbing Processes on Gas Composition

#### 5.1. Inorganic Gas Compounds

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[21] A first evaluation of the possible influence of scrubbing processes on the contents in the fumaroles of the main inorganic gas compounds (CO<sub>2</sub>, H<sub>2</sub>S, N<sub>2</sub>, Ar, H<sub>2</sub>, He and CO), as the fumarolic fluid migrates up to the surface, can be carried out by comparing the mean contents of each gas species in the fumaroles (*mean fum*) with those in the geothermal wells (*mean well*). It is worthy to point out that the composition of the whole analyzed gas species, which are constrained to a "closure" to 1,000,000  $\mu$ mol/mol, are dramatically affected by the constant sum problem [e.g., *Chayes*, 1960; *Meisch*, 1969]. Consequently, the behavior of H<sub>2</sub>O, which practically only depends

on vapor-liquid distribution during retrograde boiling of rising fluids at decreasing pressure conditions, is able to strongly control the contents of the other gas constituents being by far the most abundant compound. Therefore the (mean fum)/(mean well) ratios of inorganic gas compounds (Table 3) are more conveniently referred to the dry gas fraction. O<sub>2</sub>, whose presence is likely related to near-surface air contamination, was not considered in the present discussion. As shown in Figure 2, the values of the (mean fum)/(mean well) ratio indicate that CO<sub>2</sub> and H<sub>2</sub>S contents in the fumaroles are slightly lower than those of the geothermal wells, while CO seems, although at limited extent, depleted along the fumarolic pathways. On the contrary, N<sub>2</sub>, Ar, H<sub>2</sub> and He contents are strongly enriched in the fumaroles. Moreover, all the inorganic gas species, with the only exception of CO, are characterized by standard deviation values of the fumaroles significantly higher than those of geothermal wells (Table 3). This compositional scattering observed for the fumarolic discharges



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**Figure 2.** Histograms of the (*mean fum*)/(*mean well*) ratios of  $CO_2$ ,  $H_2S$ ,  $N_2$ , Ar,  $H_2$ , He, and CO. Gas compositions are referred to the dry gas fraction.

is likely to be ascribed to the influence of secondary processes affecting the uprising fluids. Among the possible secondary interactions able to modify the composition of the geothermal fluids, selective dissolution in water of the gas species rising along the fumarolic ducts, can be considered the most suitable physical-chemical process. Actually, the presence of aquifers overlying the geothermal reservoirs at both Berlin [Montalvo and Axelsson, 2000] and Ahuachapan-Chipilapa [Rodriguez et al., 1997] geothermal systems was evidenced. These relatively cold aquifers likely interact with the fumarolic fluids at very shallow depth, as also supported by the outlet temperature of the fumaroles (<101.7 °C), which are close to the boiling point of water at 1 atm. To verify this hypothesis the analytical data of fumaroles from Berlin-Chinameca and Ahuachapan-Chipilapa geothermal fields were compared with the expected compositions produced by dissolution-driven fractionation in water of the geothermal fluids of the two areas. Similarly to what described by Chiodini et al. [1996], who calculated the composition of a CO<sub>2</sub>rich gas phase separated in a single step from a liquid phase, we calculated the composition of a residual gas produced by dissolution of a gas phase in water on the basis of the water-vapor distribution coefficients of each gas species with respect to that of CO<sub>2</sub> by the following equation:

$$X_i/X_{CO2} = X_{o,i}X_oX_{o,CO2}/\{y \cdot [(1/S_i/S_{CO2}) - 1] + 1\}$$
(1)

where the variables are defined as follows:  $X_i$ , i-compound content after dissolution in water of the initial gas phase;  $X_{CO2}$ ,  $CO_2$  content after dissolution in water of the initial gas phase;  $X_{o,i}$ , i-compound content of the initial gas phase;  $X_{o,CO2}$ ,  $CO_2$  content of the initial gas phase;  $S_i$ , water-vapor distribution coefficient of the i-compound;  $S_{CO2}$ , water-vapor distribution coefficient of  $CO_2$ ; y, gas fraction dissolved in water.

[22] The values of  $X_{o,i}$  and  $X_{o,CO2}$  are taken from the mean composition of the production wells of Ahuachapan-Chinameca (samples 19-25; Table 1) and, separately, Berlin-Chinameca (samples 26-27 Table 1) geothermal fields, which in our model represents the initial gas phases that could be affected by dissolution during their uprise through the shallow aquifers. Starting from the selected initial gas compositions, two different series of theoretical compositions (lines A-C and B-C for the Ahuachapan-Chipilapa and Berlin-Chinameca geothermal fields, respectively) (Figures 3a-3f), are produced by substituting in equation (1) increasing y values (ranging from 0 to 0.8) to simulate increasing gas-water interaction. When the mean compositions of the Ahuachapan-Chipilapa and the Berlin-Chinameca production wells do not significantly differ, lines A-C and B-C, are coincident (Figures 3a and 3b). The  $S_i/S_{CO2}$  ratio remains almost constant at temperature  $\geq 100^{\circ}$ C [Chiodini et al., 1996], thus the solubility data used to solve equation (1) are those at 100°C [Lide, 2001].

[23] As shown in Figures 3a-3c, where CO<sub>2</sub> versus  $N_2$  (a), Ar (b) and He (c) contents are reported, at least part of the fumarolic gases tends to fit the theoretical compositions resulting from the selective dissolution process, suggesting that gas inputs from different sources, such as air dissolved into the shallow aquifers, are likely to be significant. Differently, CO contents measured in all the fumaroles are strongly lower than the expected abundances (Figure 3d), possibly because CO behavior, at slightly acidic condition, is controlled by the CO-HCOOH reaction [Shock, 1993], and this can explain the low standard deviation value in the fumaroles (0.56  $\mu$ mol/mol; Table 3) with respect to that of the geothermal wells (0.94  $\mu$ mol/mol; Table 3). On the contrary, H<sub>2</sub>S (Figure 3e) and H<sub>2</sub> (Figure 3f) seem to be in excess with respect to the dissolution trends, possibly in relation with the production of these reduced gas species during gas-water-rock interactions at relatively high temperatures, as typically occurs in volcanic-hydrothermal environment [e.g., Giggenbach, 1980, 1987, 1996].



**Figure 3.** Binary diagrams of  $CO_2$  versus (a)  $N_2$ , (b) Ar, (c) He, (d) CO, (e)  $H_2S$ , and (f)  $H_2$  contents (dry gas fraction) in fumaroles from the Ahuachapan-Chipilapa and Berlin-Chinameca geothermal fields. Expected compositions (A-C and B-C lines for Ahuachapan-Chipilapa and Berlin-Chinameca, respectively) produced by dissolution-driven fractionation process acting on geothermal fluids of the two areas are also reported.

[24] Summarizing, the simple model of selective gas dissolution in water seems to be able to describe, at least at first approximation, the effects of scrubbing processes on fumarolic fluids only for  $CO_2$ , whose chemical reactivity, in  $CO_2$ -rich geothermal fluids rising through  $CO_2$ -saturated environment at slight acidic conditions dominating the shallower hydrothermal pathways of these geothermal fields [*D'Amore and Mejia*, 1999; *Jacobo*, 2003], is relatively low, and those gas compounds that are chemically inert. Differently, the behavior of the most reactive gas species cannot easily be predicted, depending on complex chemical interaction involving gas, water and rock phases.

#### 5.2. Organic Gas Compounds

[25] As already mentioned, the fumarolic and the geothermal well discharges are characterized by the presence of many different hydrocarbons. Besides of methane,  $C_2$ - $C_9$  normal-alkanes and their isomers,  $C_3$ - $C_4$  alkenes,  $C_6$ - $C_8$  aromatics and several heterocyclics and S-substituted hydrocarbons are present (Table 2). Among this variegated group of organic gas species, hydrocarbons pertaining to the

same structural series show regular compositional variations in response to secondary processes. In fact, the (mean fum)/(mean well) ratios (calculated on the basis of the dry gas fraction) of the C<sub>2</sub>-C<sub>9</sub> normal-alkanes (Figure 4), the  $C_4$ - $C_9$  iso-alkanes and the aromatics (Figure 5) series progressively decrease as their molecular size increases. As shown in Figures 6a-6d, where the theoretical compositional trends calculated from (1) (solubility data from Lide [2001] and Cabani et al. [1981]) are also reported (lines A-C and B-C), the C2-C8 normal-alkanes contents of the fumarolic gases are less abundant than those of the geothermal wells. It must be underlined that this is exactly the contrary of what expected following the dissolution-driven mechanism. Similar results can also be obtained by considering the iso-alkanes and aromatics series (here not reported). This clearly indicates that the fractionation of normal-alkanes along the fumarolic ducts likely depends on a chemical-physical process not related to gas dissolution in water. Tentatively, the molecular dimension of each gas compound, which constitutes the main distinctive parameter for structurally homologous hydrocarbons, can be taken into account.



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**Figure 4.** Histogram of the (mean fum)/(mean well) ratios of the  $C_1$ - $C_9$  normal-alkanes series.

Actually, the values of the (mean fum)/(mean well) ratios for the  $C_n-C_{n+1}$  pairs of the normal-alkanes (Table 4) are inversely correlated ( $R^2 = 0.88$ ) with the  $C_n/C_{n+1}$  molecular volume ratios (Figure 7). Moreover, this secondary process practically has the same effects [(mean fum)/(mean well)  $\approx 1$ ] on hydrocarbons characterized by almost equal molecular volumes ( $C_n/C_{n+1}$  molecular volume ratio >0.82; Table 4). Such results can be explained when considering that, as shown by the Stokes-Einstein equation, diffusion coefficients of non-dissociating solutes in dilute solutions are mainly regulated by their molecular volumes [*Wilke and Chang*, 1955; *Bird et al.*, 1960; *Reid et al.*, 1987].

[26] Therefore the diffusion process seems to represent the main parameter controlling the fractionation of iso-structural hydrocarbons in fumarolic fluids during their uprising from the geothermal reservoirs to the surface. Accordingly, several studies [e.g., *Leythaeuser et al.*, 1979; *Hunt*, 1984; *Igari and Sakata*, 1992] have emphasized the role of diffusion as a mechanism able to control the compositional changes of light hydrocarbon ( $C_2$ - $C_7$  alkanes) in natural gases migrating from source to reservoir-type rocks.

#### 6. Geothermometry

[27] Physical-chemical conditions (temperature, pressure and redox potential) of geothermal reser-

voirs are commonly investigated on the basis of the compositional features of gas and water phases discharged by exploration and production wells [e.g., Fouillac and Michard, 1981; Arnorsson et al., 1983; Bertrami et al., 1985; D'Amore and Truesdell, 1985; Giggenbach, 1988, 1991; Chiodini and Cioni, 1989]. These studies are extremely important to assess the energy potential of geothermal fields, as well as to control the evolution of deep thermal fluids during geothermal exploitation [e.g., Fournier, 1981; Arnosson and Gunnlaugsson, 1985; D'Amore and Mejia, 1999]. The application of geothermometric techniques to naturally discharged fluids could provide these useful data even in areas where no wells have already been drilled, allowing, at least, a better evaluation of the geothermal potential of unexplored thermal systems at relatively low costs. In spite of these considerations, as also shown by the results of the present work, the chemical features of fumaroles and thermal springs seem to be deeply affected by secondary processes during the relatively slow circulation of geothermal fluids along their natural pathways.

# 6.1. Thermodynamic Equilibrium in the $H_2O-H_2-CO_2-CO-CH_4$ System

[28] The composition of hydrothermal gas discharges can usefully be represented by the  $H_2O-H_2-CO_2-CO-CH_4$  system, whose equilibrium



**Figure 5.** Histogram of the (*mean fum*)/(*mean well*) ratios of both the  $C_4$ - $C_9$  iso-alkanes and  $C_6$ - $C_8$  aromatics series.



**Figure 6.** Binary diagrams of (a)  $CH_4$  versus  $C_2H_6$ , (b)  $C_3H_8$  versus  $n-C_4H_{10}$ , (c)  $n-C_5H_{12}$  versus  $n-C_6H_{14}$ , and (d)  $n-C_7H_{16}$  versus  $n-C_8H_{18}$  (dry gas fraction) in fumaroles from the Ahuachapan-Chipilapa and Berlin-Chinameca geothermal fields. Expected compositions (A-C and B-C lines for Ahuachapan-Chipilapa and Berlin-Chinameca, respectively) produced by dissolution-driven fractionation process acting on geothermal fluids of the two areas are also reported.

constrains may be provided by the following three reactions:

$$H_2O \Leftrightarrow H_2 + 1/2O_2$$
 (2)

$$CO_2 \Leftrightarrow CO + 1/2O_2$$
 (3)

 $CO_2 + 2H_2O \Leftrightarrow CH_4 + 2O_2$  (4)

[29] Chiodini and Marini [1998] extensively investigated this restricted compositional system to evaluate the effects of secondary boiling and steam condensation processes on thermodynamic equilibrium in fluids from thermal discharges and wells

**Table 4.** Ratios Between the Mean Contents for Selected Gas Species of the Fumaroles and the Geothermal Wells From the Ahuachapan-Chipilapa, Berlin-Chinameca, and San Vicente Geothermal Fields<sup>a</sup>

	(mean well) Ratio	(mean fum) Ratio	(mean fum)/(mean well) Ratio	Molecular Volume Ratio
CH <sub>4</sub> /C <sub>2</sub> H <sub>6</sub>	7.28	35.91	4.93	0.65
$C_2H_6/\tilde{C}_3H_8$	0.933	3.440	3.69	0.72
$C_{3}H_{8}/n-C_{4}H_{10}$	3.720	6.270	1.69	0.78
$n-C_4H_{10}/n-C_5H_{12}$	4.850	3.690	0.76	0.80
$n-C_5H_{12}/n-C_6H_{14}$	1.840	1.160	0.63	0.83
$n-C_6H_{14}/n-C_7H_{17}$	4.980	4.890	0.98	0.85
$n-C_7H_{16}/n-C_8H_{18}$	1.810	1.500	0.83	0.86
$n-C_8H_{18}/n-C_9H_{20}$	2.650	2.980	1.12	0.88

<sup>a</sup> The (mean fum)/(mean well) and the molecular volume ratios were also reported.



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**Figure 7.** Binary diagram of molecular volume ratios versus (*mean fum*)/(*mean well*) ratios for the  $C_n-C_{n+1}$  pairs of the normal-alkanes series.

seeping out in a wide range of volcanic and nonvolcanic environments. These authors have evidenced that the H<sub>2</sub>/H<sub>2</sub>O, CO/CO<sub>2</sub> and CH<sub>4</sub>/ CO<sub>2</sub> log-ratios, which constitute the most suitable geothermometers for hydrothermal fluids [*Giggenbach*, 1987, 1991], strongly depend on (1) different kinetic responses of each compound to changes of thermodynamic parameters as thermal fluids rise up to the surface, (2) vapor-liquid distribution coefficients of the different gas species, and (3) fraction of separated vapor or condensed steam.

[30] Following a similar approach, the analytical data of fumaroles and geothermal wells from El Salvador geothermal fields are graphically compared with the computed theoretical compositions of gases that have attained chemical equilibrium at different temperatures (150, 200, 250, 300 and 350°C) in (1) pure saturated vapor (vapor), (2) liquid (liquid), and (3) coexisting vapor plus liquid phases, assuming that redox conditions are governed by the  $FeO/FeO_{1.5}$  buffer proposed by Giggenbach [1987]. In the  $log(CH_4/CO_2)$  versus log(CO/CO<sub>2</sub>) diagram (Figure 8) all gas samples plot out of the theoretical grid between the vapor and the liquid lines for hydrothermal fluids. This result may be due to the different kinetics characterizing the chemical behavior of CO and CH<sub>4</sub>. The former is, as well as  $H_2$ , a fast-reacting species, while the latter is one of the slowest species to equilibrate [Nehring and D'Amore, 1984; Giggenbach, 1987; Chiodini et al., 1993]. Moreover, it has to be considered that redox conditions of the geothermal reservoirs may not be controlled by a single buffer system. Low CH<sub>4</sub>/ CO<sub>2</sub> ratios (and consequently unrealistic high CH<sub>4</sub>-CO<sub>2</sub> equilibrium temperature), whose dependence on  $fO_2$  is four times larger than that of the  $CO/CO_2$  ratio (equations (3) and (4)), could be due to more oxidizing conditions with respect to those constrained by the FeO/FeO<sub>1.5</sub> buffer, possibly in relation to magmatic-related fluid inputs into the roots of the geothermal systems, as suggested for other volcanic systems (i.e., Phlegrean Fields, Ischia, Teide) by Chiodini and Marini [1998]. Ahuachapan-Chipilapa, Berlin-Chinameca and San Vicente geothermal fields are indeed located in active volcanic areas, as also supported by the mantle signature of the helium isotopic ratios (up to 7.1 R/Rair) [Snyder et al., 2003]. Therefore the presence of deep-circulating SO<sub>2</sub>-rich fluids, able to interact with the geothermal reservoirs, cannot be excluded, although SO<sub>2</sub> was detected in neither the discharging fluids nor the geothermal wells (Table 1), possibly because, as previously suggested, this highly soluble compound is totally dissolved into the geothermal liquiddominated system.



**Figure 8.**  $Log(CH_4/CO_2)$  versus  $log(CO/CO_2)$  binary diagram. The computed theoretical compositions (FeO-FeO<sub>1.5</sub> buffer system) of (1) pure saturated vapor, (2) vapor separated from liquid in a single step, and (3) liquid phases [*Chiodini and Marini*, 1998] are also reported. Open triangle, fumarole; open circle, geothermal well.

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**Figure 9.**  $Log(H_2/H_2O)$  versus  $log(CO/CO_2)$  binary diagram. The computed theoretical compositions (FeO-FeO<sub>1.5</sub> buffer system) of (1) pure saturated vapor, (2) vapor separated from liquid in a single step, and (3) liquid phases [*Chiodini and Marini*, 1998] are also reported. Symbols as in Figure 8.

[31] In the  $log(H_2/H_2O)$  versus  $log(CO/CO_2)$  diagram (Figure 9) gas samples plot within the expected compositional field for vapors produced through boiling of a liquid phase at initial temperature ranging between 180 and 250°C. Such temperatures are significantly lower than those estimated for Ahuachapan-Chipilapa geothermal fluids ( $\approx 260^{\circ}$ C) [Truesdell et al., 1989] and measured in the deep wells from the Berlin geothermal field (up to 310°C) [D'Amore and Mejia, 1999], likely due to partial reequilibration of both the H<sub>2</sub>-H<sub>2</sub>O and CO-CO<sub>2</sub> pairs, indicating that both the fumaroles and the geothermal wells show clues of compositional readjustment at decreasing temperature and pressure conditions during fluid rise. Furthermore, the large variation shown by the  $H_2/$ H<sub>2</sub>O ratio (more than 2 log-units) (Figure 9) seems to be mainly depending on the strong influence of secondary interactions (i.e., gas-water-rock reactions) on H<sub>2</sub> contents in fumaroles (Figure 2 and Table 3). Similarly, the CO/CO<sub>2</sub> log-ratios are likely dependent on CO-consumption at shallow depth due to formiate production from CO [Shock, 1993], a process that may have continued in the time-interval (about two weeks) between the collection and the analysis of gas samples, leading to a general lowering of the CO-CO<sub>2</sub> equilibrium temperatures (Figure 9).

[32] In conclusion, the different chemical-physical behavior of the various compounds involved seems to imply severe limitations to the use of the H<sub>2</sub>O-H<sub>2</sub>-CO<sub>2</sub>-CO-CH<sub>4</sub> system for geothermometric purposes, especially when analytical data are referred to the composition of naturally discharged fluids.

# 6.2. Thermodynamic Equilibria Among Hydrocarbons

[33] Thermodynamic properties and chemical behavior of aqueous organic species at hydrothermal conditions were extensively investigated only in recent times [Shock and Helgeson, 1990; Shock, 1990a]. Shock [1990b] first claimed that these compounds may attain metastable equilibrium over geologically significant periods of time. Accordingly, laboratory experiments, conducted at 300 to 350°C and 350 bar to examine chemical interactions of light hydrocarbons with water under the redox control of Fe-bearing mineral buffers, have demonstrated that alkene-alkane, alkene-ketone and alkene-alcohol pairs are able to achieve metastable equilibrium states within the timescale from hundreds to thousands of hours [Seewald, 1994, 2001]. In relation to the results of these investigations, the possible application of organic gas composition to geothermometry has been extensively debated [e.g., Sugisaki and Nagamine, 1995; Taran and Giggenbach, 2003; Capaccioni et al., 2004]. Several authors [e.g., Giggenbach, 1997; Taran and Giggenbach, 2003] have stressed the fact that hydrolysis reactions regulating the  $C_1$ - $C_2$ - $C_3$ - $C_4$ alkane system in natural environment are not reversible processes, since the reversibility of the stepwise breakage of C-C bonds is largely limited by a kinetic barrier [Stocchi, 1991]. Barker and Takach [1992] suggested that the production of alkanes is not thermodynamically controlled, although, at high temperatures, this process possibly converges to equilibrium. On the other hand, Darling [1998], assuming a thermal breakdown mechanism for the production of CH<sub>4</sub> from C<sub>2+</sub> alkanes, formulated an empirical relationship between the CH<sub>4</sub>/C<sub>2</sub>H<sub>6</sub> ratio and the temperature of deep thermal fluids that moderately well fits a range of hydrothermal systems worldwide. Furthermore, Capaccioni and Mangani [2001], on the basis of the composition of La Solfatara volcano fumaroles (Phlegrean Fields, Italy), stressed that the C1-C2-C3 alkanes, characterized by similar solubility [Lide, 2001], for hydrothermal fluids with relatively long residence time at depth and in presence of abundant catalysts (such as free acids, allumosilicates and sulfur species), may be



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**Figure 10.** Log(CH<sub>4</sub>/C<sub>2</sub>H<sub>6</sub>) versus C<sub>2</sub>H<sub>6</sub>/C<sub>3</sub>H<sub>8</sub>) binary diagram. Isotherms (in °C) refer to the equilibrium:  $2C_3H_8 = C_2H_6 + CH_4$ . Symbols as in Figure 8.

thermodynamically controlled, in gases released from a single liquid phase, by the following pressure-independent equilibrium reaction:

$$2C_2H_6 \Leftrightarrow C_3H_8 + CH_4 \tag{5}$$

[34] According to thermodynamic data [*Reid et al.*, 1987; *Barin*, 1989], the temperature dependence of the equilibrium constant of reaction (5) is

$$\log(CH_4/C_2H_6) - \log(C_2H_6/C_3H_8) = -0.0828 + 457.42/T$$
(6)

[35] As shown by the  $log(CH_4/C_2H_6)$  versus  $\log(C_2H_6/C_3H_8)$  diagram (Figure 10), geothermal gases plot within the isotherms 220-260°C (dashed lines) of the  $CH_4$ - $C_2H_6$ - $C_3H_8$  equilibrium, in agreement with the temperatures measured at depth ranging from 1500 to 2400 m in the Berlin geothermal field, and slightly higher than those found in the Ahuachapan-Chipilapa geothermal field at shallower depth (600-1500 m) [D'Amore and Mejia, 1999] and with those calculated with the Na-K-Ca geothermometer [Fournier and Truesdell, 1973] by Snyder and Fehn [2002]. This represents an important result because it seems to constitute one of the rare examples of thermodynamic equilibrium attained among the C<sub>1</sub>-C<sub>2</sub>-C<sub>3</sub> alkanes [Sugizaki and Nagamine, 1995; Capaccioni and Mangani, 2001]. A second fundamental indication is that gases from both fumaroles and geothermal wells are in the same range of equilibrium temperatures (Figure 10), although, as previously observed (Figures 4 and 5), hydrocarbon contents in fumaroles are strongly affected by secondary interactions. Actually, the effects of gas diffusion, which seems to represent the main process able to control the (mean fum)/(mean well) ratios of the iso-structural hydrocarbons of geothermal fluids rising through shallow aquifers, are to be considered negligible for the  $(CH_4/C_2H_6)/(C_2H_6/C_3H_8)$ log-ratios since the  $CH_4/C_2H_6$  and the  $C_2H_6/C_3H_8$ molecular volume ratios are very similar (0.65 and 0.72, respectively; Table 4). Differently, the CH<sub>4</sub>/C<sub>2</sub>H<sub>6</sub> and C<sub>2</sub>H<sub>6</sub>/C<sub>3</sub>H<sub>8</sub> log-ratios, considered separately, are significantly higher in the fumaroles than in the geothermal wells (Figure 10), depending on the largely different molecular volumes of  $CH_4$ ,  $C_2H_6$  and  $C_3H_8$  (42.1, 65.1 and 90.5, respectively; Table 3).

[36] A similar approach can be adopted to investigate the  $C_1$ - $C_2$ - $C_3$ - $C_4$  alkane system, whose internal equilibrium is regulated by the following reaction [*Capaccioni and Mangani*, 2001]:

$$CH_4 + n - C_4 H_{10} \Leftrightarrow C_2 H_6 + C_3 H_8 \tag{7}$$

[37] The temperature dependence of the equilibrium constant of reaction (7) (at  $T > 200^{\circ}C$ ) is given by

$$\log(CH_4/C_2H_6) - \log(C_3H_8/n-C_4H_{10})$$
  
= -0.0567 + 477/T (8)

[38] As shown in Figure 11, both geothermal wells and fumaroles are scattered in a wide area, indi-



**Figure 11.** Log(CH<sub>4</sub>/C<sub>2</sub>H<sub>6</sub>) versus  $C_3H_8/n-C_4H_{10}$ ) binary diagram. Isotherms (in °C) refer to the equilibrium: CH<sub>4</sub> + n-C<sub>4</sub>H<sub>10</sub>  $\Leftrightarrow$  C<sub>2</sub>H<sub>6</sub> + C<sub>3</sub>H<sub>8</sub>. Symbols as in Figure 8.



cating equilibrium temperatures ranging from 50 to >700°C. This result may be ascribed to two possible reasons: (1) reaction (7) has not attained a complete equilibrium, possibly in relation to further chemical reactions involving  $n-C_4H_{10}$ , and (2) secondary processes. Concerning the first hypothesis, we believe that the apparent disequilibrium of reaction (7) is mainly due to the interaction between  $n-C_4H_{10}$  and its isomer,  $i-C_4H_{10}$ . It is worthy of note that the  $CH_4/C_2H_6$  molecular volume ratio is significantly different with respect to that of  $C_3H_8$ - $n/C_4H_{10}$  (0.65 and 0.78, respectively; Table 4); thus the composition of the  $C_1-C_4$  alkanes may also depend on the influence of the diffusion process.

[39] Further reactions among light hydrocarbons that can usefully be utilized for evaluating deep temperatures in geothermal and volcanic systems are those of de-hydrogenation processes [e.g., *Capaccioni and Mangani*, 2001; *Tassi et al.*, 2005b], which result in saturated-unsaturated conversion of the alkane-alkene pairs without strong structural changes.

[40] De-hydrogenation reaction of the  $C_3$  alkenealkane pair is given by

$$C_3H_8 \Leftrightarrow C_3H_6 + H_2 \tag{9}$$

whose temperature dependence is given by

$$\log(C_3H_6/C_3H_8) + \log fH_2 = 7.15 - 6,600/T$$
(10)

[41] As shown by (10), the relative abundances of  $C_3H_6$  and  $C_3H_8$  are regulated, besides of the temperature, by the hydrogen fugacity, which in turn is instantaneously governed by redox conditions. As suggested by *Giggenbach* [1987], the most suitable parameter to describe redox potentials of natural fluids is:

$$R_{\rm H} = \log(f H_2 / f H_2 O) \tag{11}$$

[42] The  $R_H$  values referring to the FeO-FeO<sub>1.5</sub> couple, which is considered the most suitable redox buffer system for hydrothermal fluids [*Giggenbach*, 1987], are fixed by the generalized reaction [*Giggenbach et al.*, 1986]:

$$H_2O + 2FeO \Leftrightarrow H_2 + 2FeO_{1.5}$$
(12)

[43] However, as suggested by the distribution of gas samples in Figure 8, the redox conditions dominating the geothermal reservoir of both Ahuachapan-Chipilapa and Berlin-Chinameca geothermal fields are likely more oxidative than those expected when the FeO-FeO<sub>1.5</sub> buffer is predominating. Therefore the redox buffer system involving hematite and magnetite (HM), which is possibly in equilibrium with geothermal gases at relatively high oxidation potential [*Giggenbach*, 1987], was also adopted. The  $R_H$  values referring to the hematite-magnetite couple are fixed by the reaction

$$H_2O + 2Fe_3O_4 \Leftrightarrow H_2 + 3Fe_2O_3 \tag{13}$$

[44] Hence, assuming that changes of  $log f H_2 O$  with temperature are closely approximated by the following equation [*Giggenbach*, 1980]:

$$\log f H_2 O = 5.51 - 2048/T \tag{14}$$

and using the temperature dependences of the equilibrium constants of reactions (12) and (13) proposed by *Giggenbach* [1987], hydrogen fugacity can be linked to temperature through the following equations:

$$\log f H_2 = 2.71 - 2048/T \tag{15}$$

$$\log f H_2 = 0.91 - 2318/T \tag{16}$$

[45] Finally, by combining (10) with (15) and (16), the theoretical relationship between the  $C_3H_6/C_3H_8$  ratios and temperature for gases equilibrated at the typical redox conditions for hydrothermal and volcanic environments, respectively, can be obtained.

[46] As shown in the  $\log(C_3H_6/C_3H_8)$  versus temperature diagram (Figure 12) (where temperature values are those calculated with the  $C_1$ - $C_2$ - $C_3$ alkane geothermometer, since alkanes and alkenes pertain to the same compositional sub-system and are supposed to be produced by a common source), geothermal gases are clustered in a narrow area at higher oxidizing conditions even than those of the HM redox buffer, suggesting that (1) as already observed in volcanic gases [Taran and Giggenbach, 2003], reaction (9) is really able to control the  $C_3H_6/C_3H_8$  ratios and (2) the  $C_3H_6-C_3H_8$  couple equilibrates at redox conditions that are to be considered unusual for geothermal systems [e.g., Giggenbach, 1980, 1987]. Magmatic-related fluid inputs able to affect the redox conditions of the Ahuachapan-Chipilapa, Berlin-Chinameca and San Vicente geothermal systems were already invoked to justify gas distribution in the binary diagram (Figure 8) describing the thermodynamic equilibria of the CH<sub>4</sub>/CO/CO<sub>2</sub> redox system. Accordingly,



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**Figure 12.**  $Log(C_3H_6/C_3H_8)$  versus  $(C_1-C_2-C_3)$ -calculated temperature diagram. Solid lines represent the positions of the GT and HM redox buffer systems. Symbols as in Figure 8.

the high  $C_3H_6$ - $C_3H_8$  ratios of Laguna Alegria and Oyon Crater (samples 11 and 12; Figure 12), which represent the most recent craters of the Tecapa-Berlin volcanic system [*D'Amore and Mejia*, 1999], are possibly due to particularly conspicuous addition of highly oxidizing hot fluids, whose occurrence is also supported by both the presence of oxygen-substituted hydrocarbons (C<sub>4</sub>H<sub>4</sub>O and C<sub>5</sub>H<sub>6</sub>O; Table 2), typically produced at high temperature [*Montegrossi et al.*, 2003], and the relatively high H<sub>2</sub> and CO contents.

[47] It must be underscored that the  $C_3H_6/C_3H_8$  logratios in the fumaroles and the geothermal wells are in the same range (Figure 12). Therefore the  $C_3H_6$ - $C_3H_8$  geothermometer, as well as that of the  $C_1$ - $C_2$ - $C_3$  alkanes, seems to be not significantly affected secondary processes occurring along the fumarolic pathways, likely due to the minimum difference between the molecular volumes of these two compounds ( $C_3H_6/C_3H_8$  molecular volume ratio = 0.91). This consideration confirms once again that a strong relation exists between the diffusion process and the (*mean fum*)/(*mean well*) ratios.

[48] Among the possible chemical reactions involving the  $C_4$  unsaturated-saturated pairs, de-hydrogenation of the iso- $C_4$  alkane to form the iso- $C_4$  alkene can be considered:

$$(CH_3)_3 CH(i\text{-butane}) \Leftrightarrow (CH_3)_2 C = CH_2(i\text{-butene}) + H_2$$
  
(17)

[49] The temperature dependence of the equilibrium constant of reaction (17) is given by

$$8.18 - 5,780/T - 270,398/T^{2}$$
  
= log[(CH<sub>3</sub>)<sub>2</sub>C = CH<sub>2</sub>]/[(CH<sub>3</sub>)<sub>3</sub>CH] + log*f*H<sub>2</sub>  
(18)

[50] The theoretical compositions for gases equilibrated at redox conditions governed by the FeO/  $FeO_{1,5}$  and the HM buffer systems, respectively, were obtained by combining (18) with (15) and (16), respectively. As shown in Figure 13, the  $i-C_4H_8/$ i-C<sub>4</sub>H<sub>10</sub> ratio, as that of the C<sub>3</sub>-C<sub>3</sub> alkane-alkene pair, seems to be established at relatively high oxidizing conditions, although gas samples are significantly scattered along the y axis, possibly due to the fact that reaction (17) has not attained thermodynamic equilibrium in the considered temperature range. The molecular volumes of the two iso-C<sub>4</sub> hydrocarbons are indeed almost identical (Table 3), thus we can hypothesize that the diffusion process is not able to significantly affect the  $i-C_4H_8/$  $i-C_4H_{10}$  ratio. Nevertheless, it seems not reasonable that two almost identical chemical processes, i.e., the de-hydrogenation reactions of the C<sub>3</sub> and the C<sub>4</sub> alkane-alkene pairs, can show a distinct thermodynamic response. Consequently, as also supported by the lack of equilibrium of the  $C_1$ - $C_2$ - $C_3$ - $C_4$  alkane system (Figure 11), the interaction between the two C<sub>4</sub>-isomers, i-C<sub>4</sub>H<sub>10</sub> and n-C<sub>4</sub>H<sub>10</sub>, remains the most



**Figure 13.** Log(iso- $C_4H_8$ /iso- $C_4H_{10}$ ) versus ( $C_1$ - $C_2$ - $C_3$ )-calculated temperature diagram. Solid lines represent the positions of the GT and HM redox buffer systems. Symbols as in Figure 8.

likely mechanism able to explain the gas distribution shown in Figure 13.

### 7. Conclusions

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[51] Temperature-dependent interactions between gas species stored within geothermal reservoirs, where fluids have long residence times and the physical-chemical conditions (temperature, pressure) are particularly favorable to the proceeding of chemical reactions, are likely to be able to achieve a complete equilibrium. This is confirmed by the reliable temperature estimations commonly obtained by applying the geothermometric techniques based on the composition of the deep production wells [e.g., Arnorsson et al., 1983; Bertrami et al., 1985, Giggenbach, 1991], which are likely very similar to that thermodynamically established at depth since exploited fluids rapidly move toward surface and are almost isolated by the shallow environment. On the contrary, it is reasonable to suppose that the compositional features of geothermal reservoirs are rarely maintained by fumarolic discharges, mainly due to the influence of secondary processes that may take place during the slow gas ascension along the natural pathways. The composition of naturally discharging fluids from fumaroles of Auhachapan-Chipilapa and Berlin-Chinameca geothermal fields, when compared to that of the geothermal wells of the same areas, have indeed shown that (1) dissolution-driven fractionation due to the interaction of geothermal fluids with shallow aquifers is able to control, at least partially, N<sub>2</sub>, Ar, He and CO<sub>2</sub> contents in fumarolic gases; (2) fumarolic gases, with respect to gases from geothermal wells, are strongly enriched in H<sub>2</sub> and slightly depleted in CO and H<sub>2</sub>S, likely due to complex secondary gas-water-rock chemical reactions; (3) organic gases of geothermal fluids are significantly depleted at relatively shallow depth by scrubbing processes (i.e., dissolution in shallow aquifers); (4) the relative abundances of the structurally homogeneous gases pertaining to the C2-C9 normal-alkane, iso-alkane and aromatic series in response to secondary interactions appear to be mainly regulated by the diffusion velocity of gases through shallow aquifers, a parameter that is function of the molecular volume of each gas species; and (5) the thermochemical equilibrium of reactions among hydrocarbons characterized by similar molecular dimensions and structure, i.e., the C<sub>3</sub>-C<sub>3</sub> and the C<sub>4</sub>-C<sub>4</sub> alkane-alkene pairs, as well as the very rare metastable equilibrium [Capaccioni and Mangani, 2001] of the chemical reaction among the  $C_1$ - $C_2$ - $C_3$  alkanes, whose behavior is commonly that of a non-reversible process [*Taran and Giggenbach*, 2003], seems to be attained. Therefore the chemical equilibria among light hydrocarbons can constitute a useful tool to provide reliable estimations of geothermal reservoir temperature and dominating redox conditions, especially during the exploration phase of promising areas for geothermal resources and for the geochemical monitoring of active volcanoes, where only natural gas emissions are available.

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