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Total- and semi-bare noble metal nanoparticles@silica core@shell catalysts for hydrogen generation by formic acid decomposition

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Abstract

Catalysts are involved in a number of established and emerging chemical processes as well as in environmental remediation and energy conversion. Nanoparticles (NPs) can offer several advantages over some conventional catalysts, such as higher efficiency and selectivity. Nowadays, versatile and scalable nanocatalysts that combine activity and stability are still lacking. Here, we report a comprehensive investigation on the production and characterization of hybrid nano-architectures bringing a partial or total bare surface together with their catalytic efficiency evaluation on, as a proof-of-concept, the formic acid decomposition reaction. In this regard, formic acid (FA) is a convenient and safe hydrogen carrier with appealing features for mobile applications, fuel cells technologies, petrochemical processes and energetic applications. Thus, the design of robust catalysts for FA dehydrogenation is strongly demanded. Due to this, we produced and evaluated nano-architectures with various equilibrium between the size-increase of the active part and the barer catalytic surface. Overall, this work paves the way for the development of new approaches for green energy storage and safe delivery.

Keywords Gold · Nanomaterials · Silica · Formic acid · Hydrogen

1 Introduction

One of the main fields in which engineered nanomaterials demonstrate their potential is in catalysis [1–4]. In particular, metal nanoparticles (NPs) are of special interest due to their increased catalytic activity with respect to bulk materials. On the other hand, their size may cause difficulties in handling and employing them in traditional industrial processes [5].

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Indeed, NPs can be affected by sintering/stability and recovery issues [6]. An elegant strategy to both reduces NPs sintering while increasing their lifetime is the core@shell design, in which the active part is confined in the core and an external shell protect the catalyst [7]. This approach has the intrinsic advantage to increase the NPs recyclability and stability to coalescence due to the protective shell [8]. Moreover, the core@shell approach is usually versatile due to the easily tunable behaviors associated with the composition of the NPs [7, 9, 10]. On the other hand, the confinement of the active part reduces its accessibility and decreases the overall catalytic activity for some reactions [8]. In this context, investigations on the modulation of the catalytic activity associated to structural modifications of core@shell NPs are pivotal to recognize the best structural equilibrium between the building blocks.

In this work, three core@shell nanocatalysts have been systematically investigated in order to maximize both the stability and catalytic activity over, as model reaction, the formic acid (FA) decomposition. FA is one of the major products from biomass processing and from a variety of chemical reactions based on methyl formate hydrolysis or CO₂ hydrogenation [11]. Noticeably, FA decomposition is a virtuous, safe, cyclic, and convenient reaction for hydrogen delivery and



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generation. Indeed, hydrogen stored in FA can be released in situ by catalytic dehydrogenation [12]. It is worth to remember that the FA dehydration requires a CO resistant catalyst as gold because it shows better resistance to deactivation and poisoning with respect to Pt or Ru [13].

In this regard, we have employed as a first approach to the FA decomposition the passion fruit-like nano-architecture (NAs) [14]. NAs are silica nanocapsule comprising 3 nm ultrasmall gold NPs embedded and stabilized between two ionic polymers [15]. The passion fruit NAs are scalable, standardized, cheap and easily tunable during the synthesis by adapting the standard protocols [14, 16, 17]. From NAs, other two yolk-shell like nanostructures have been generated by an annealing process in air. The stabilizing agents (polymers) degradation and the annealing temperature enable the controlled metal sintering processes, with a consequent increase in NPs size. During the annealing treatments, nanomaterials with size-increased and bare active parts have been produced, the MultiCore (mc) and SingleCore (sc) NAs, thanks to polymers burning and ultrasmall metal NPs melting and re-condensation. Ideally, bare gold NPs comprised in NAs should present the maximum number of exposed active centers, resulting in a nanocatalyst that jointly combine efficiency with stability [18]. Here, the hybrid nano-architectures bringing a partial or total bare surface have been comprehensively characterized and their efficiency over the FA decomposition compared. This systematic work paves the way for the rational design of a low-cost versatile family of heterogeneous hybrid nanocatalysts for green energy storage and safe delivery of hydrogen.

2 Results & discussion

2.1 Multicore (mc) and Singlecore (sc) NAs synthesis

A schematic representation for standard NAs production is reported in Fig. 1a [18]. The ultrasmall AuNPs (3 nm) are produced by a fast reduction of HAuCl₄ (tetra chloroauric acid) by NaBH₄ (sodium borohydride) in presence of PSS (poly(sodium 4-styrene sulfonate)). The solution turns instantly from bright yellow to dark red/brown and, in 10 min, it becomes brilliant red due to the growth of 3 nm gold NPs. When PLL (poly-L-lysine) solution is added, NPs are assembled in spherical arrays by a controlled aggregation achieved by ionic interactions between PSS and PLL [17–19]. The polymer arrays are purified by centrifugation and employed in a Stöber reaction to form the silica shell. During the reaction, TEOS molecules tend to condense, crosslink and form a polysiloxane network covering the gold/polymers arrays, as reported by Cassano et al. [14]. After the Stöber reaction, the resulting standard NAs are centrifuged to discard the unreacted species. NAs are resuspended in EtOH by



sonication and the nano-architectures bigger than about 150 nm removed by precipitation (Fig. S1). Then, collected particles are freeze-dried overnight. Usually, about 1.5 mg of a shiny red powder is obtained from one-shot synthesis. This synthetic protocol can be actually scaled up to 10X in order to obtain up to 15 mg of NAs. The product remains stable for 1 year if stored in the dark at 10 °C [18]. Remarkably, the reaction can be modulated in order to prepare NAs containing Ag, Pt or mixed metals [14], and their raw production cost reduced by replacing PLL with PEI (polyethyleneimine) [19].

NAs can be converted in mcNAs and scNAs by a controlled annealing treatment of the freeze-dried NAs powders. mcNAs and scNAs comprise partially or totally bare gold NPs, which should maximize the number of active centres exposed on the metal surface [6]. Freeze-dried NAs appear as a ruby red powder (Fig. 1b). Interestingly, variations of the annealing treatments generate different products (Fig. S2). The mcNAs are obtained by annealing NAs by the "single step-like" heating ramp (the temperature reaches 350 °C in 15 min and is kept constant for 6 h). After the thermal treatment, mcNAs look as a black powder (Fig. 1b). The black color can be associated to the presence of unburned carbon compounds as a consequence of a not complete polymers oxidation [20]. Moreover, the unburned carbon compounds can act as physical stabilization agents for metal NPs that experience a partial sintering during the annealing treatment, which produces multinucleated NAs with metal cores of less than 10 nm in diameter (Table 1) [21].

The *sc*NAs are obtained by NAs annealing following the "two step-like" heating ramp (Fig. S2). Briefly, the temperature reaches 200 °C in 15 min, it is kept constant for 120 min, increased up to 400 °C in 15 min, still increased to 600 °C with a heating rate set at 100 °C h⁻¹, and maintained at 600 °C for 105 min. After the thermal treatment, *sc*NAs are collected as a pink powder (Fig. 1b). The *sc*NAs pink color can be associated to the metal NPs size that changed during the treatment and to the changed dielectric environment [22]. Indeed, *sc*NAs are composed by a single and bare gold nanoparticle of about 20 nm inside the silica capsule (Table 1).

2.2 mcNAs and scNAs characterization

The three species of NAs have been comprehensively characterized by using TEM imaging for the morphologic investigation (Fig. 1b); FTIR (Fourier Transform InfraRed) spectroscopy (Fig. 2a) and EELS (Electron Energy Loss Spectroscopy) (Fig. 2b) to check polymers behavior induced by the annealing; ICP-MS (Inductively Coupled Plasma Mass Spectrometry) for elemental quantitative analysis (Table 1); powder XRD (X-Ray Diffraction) (Fig. 2b) for NAs phase identification and characterization.



Fig. 1 a General synthesis scheme for the composition of NAs. 3 nm ultrasmall gold nanoparticles are stabilized by poly(sodium 4-styrene sulfonate) and assembled in polymer arrays by employing poly(L-lysine). Then, the templates are covered by a silica shell [18]. NAs can be further converted in *multicore (mc)* or *singlecore (sc)* NAs by an annealing

process. *mc*NAs and *sc*NAs comprise partially or totally bare gold NPs. **b** In each row are reported a photo of the NAs powders (left), and two bright field TEM images at different magnifications, a larger area at lower magnification (center) and a higher magnification taken on one single particle (right). Scalebars are 200 nm (center) and 100 nm (right)

FTIR spectroscopy provides molecular details about functional groups comprised in the nano-architectures. The FTIR spectra of NAs, PLL and PSS are reported together with their peak's assignment in Fig.S3 and Table S4. The FTIR spectra of NAs, *mc*NAs and *sc*NAs are reported in Fig.2a.

In the NAs spectrum, two distinct sets of relevant peaks can be observed. The first, it is the C=O amide group stretching



Silica cansule diameter (nm)	Shell thic	zness (nm)
performed on at least 50 NAs collected by TEM. Quantitative l	CP-MS	INAS and the total v
the silica shell (second column), and average diameter of	of gold	centage is referred t
Table 1 Average diameters of NAs (first column), average thick	cness of	analyses of gold co

analyses of gold comprised in NAs (last column). The Au weight percentage is referred to the ratio between the weight of Au contained in the NAs and the total weight of the freeze-dried samples

	Silica capsule diameter (nm)	Shell thickness (nm)	AuNPs size (nm)	Au weight %
NAs	110 ± 19	33 ± 4	2.8 ± 0.5	$7.4\pm0.6\%$
mcNAs	122 ± 21	34 ± 3	8 ± 2	$8 \pm 1\%$
scNAs	123 ± 34	25 ± 3	18 ± 9	$7.3\pm0.7\%$

peaked at 1650 cm⁻¹, which derives from PLL, combined with the water bending peak at 1640 cm^{-1} [23]. The second, it is the Si-O stretching band between 1500 and 800 cm⁻¹ associated to the silica shell, which is very intense respect to the amide signal. This set is formed by three main peaks, which are at 1157, 1054, 940 cm⁻¹ [23, 24]. The PSS peaks are weak and masked in the NAs spectrum. Indeed, the PSS degradation cannot be directly confirmed from the IR spectra in mcNAs and scNAs. On the other hand, the C=O peak decrease gradually in intensity from NAs to mcNAs and scNAs. This result may suggest the gradual PLL degradation promoted by the annealing process but cannot be confirmed because of the presence of the water bending peak jointly combined with the low intensity variation. The stretching mode peaked at 1157 cm⁻¹ for the Si-O bands decreases gradually in intensity up to become a shoulder. Also, the 940 cm⁻¹ peak gradually decreases in intensity from NAs to scNAs. These spectral changes can be associated to structural modifications of the silica shell promoted by the annealing process, such as a gradual silica crosslink and reorganization [25].

The EELS spectrum of scNAs has been collected to further investigate the polymers oxidation and partial escape during the annealing process (Fig. 2b). This technique measures the energy distribution of electrons that have interacted with the sample and their energy loss due to inelastic scattering [26]. Thus, elemental analysis can be performed by detecting in the ELLS spectrum the energy loss peaks corresponding to the ionization energies of the different elements (ionization edges) [26]. This technique is particularly efficient for light elements. At 165 eV, the sulfur L edge peak is weak but present, highlighting a possible presence of S species in scNAs. This finding may be associated to a partial escape of sulfur produced by the degradation of the PSS sulfonate groups due to its strong affinity with gold [21]. Instead, the nitrogen K edge peak at 400 eV is completely absent. By combining both the EELS and FTIR results, the PLL degradation and its products escape from *sc*NAs is confirmed. The carbon signal in the spectrum is mainly due to the carbon film of the sample holder grid, while the oxygen signal comes from the silica shell.

Powder XRD has been employed to collect qualitative structural information about NAs, *mc*NAs and *sc*NAs and



their components. Their PXRD patterns are reported in Fig. 2c. NAs pattern (green) display the silica characteristic peak at 2θ value of 22.74° , which confirms the amorphous nature of the silica shell [27]. Four broad peaks are present at 2θ values of 38.49°, 44.06°, 65.51° and 78.49°, which can be indexed as the 111, 200, 220 and 311 reflections of face centred cubic (FCC) gold. The broadness of these peaks reveals the nanometric size of the ultrasmall AuNPs [28]. Interestingly, the silica peak of mcNAs and scNAs experiences a shift up to 21.46°. Taken together with the FTIR spectra, this result confirms the silica shell reorganization induced by the annealing process [25, 29]. This sharpening allows to see in mcNAs and scNAs the weak 222 reflection of gold FCC lattice at 81.7° [30, 31]. The gradual gold peaks sharpening, from NAs to mcNAs and scNAs, is related to the increasing size of the coherent crystalline domains of gold during the annealing, which tend to grow up to about 20 nm in the scNAs [32].

2.3 Formic acid catalytic decomposition

Formic Acid (HCOOH or FA) is a convenient and safe H_2 carrier useful in mobile applications, fuel cells technologies, petrochemical processes, and energy delivery and conversion [33]. On this hand, FA is considered a good candidate to satisfy the increasing demands of high purity H_2 [34, 35]. In this context, FA controlled, efficient and selective dehydrogenation by a robust catalyst is strongly demanded [5]. Pt, Ir, Pd, Ru, Rh catalyst are not suitable choices for this reaction due to the presence of an equilibrium between FA dehydrogenation and dehydration. FA dehydration tends to form $H_2O + CO$. CO levels at temperature close to 100 °C become relevant and usually deactivate the catalyst [33].

Several groups have investigated the efficiency of homogeneous or heterogeneous catalysts for FA decomposition. Coffey et al. describe a pioneering approach by employing iridium phosphine complex for the decomposition of FA in acetic acid at about 110 °C [36]. Furthermore, many transition metal complexes have been tested in this model reaction, such as [Ru2(μ -CO)(CO)4(μ -dppm)2] [37], [RhCp*(bpy)Cl]Cl [38], [Fe(BF₄)₂]×6H₂O [39], [IrCp*(4,4'-hydroxy-2,2'bipyridine)] [40]. Generally, the main goal of these



Fig. 2 a FTIR spectra of NAs (green), mc (red) and sc (blue) NAs. Spectrum resolution about 1.9 cm⁻¹. **b** scNAs EELS spectrum. Peak labels are superimposed with the spectrum and assigned by comparison with the EELS atlas database. C) NAs (green), mc (red) and scNAs (blue) superimposed powder XRD patterns

investigations was to achieve the higher turnover frequency at the lowest temperature [33]. Concerning heterogeneous catalysts, mono- and bi-metallic catalysts have been the most widely investigated for FA decomposition, among which PdAu/C-CeO₂ [41], Pd/C [42], Ag@Pd/C [43]. Ojeda et al. [44] reported that finely dispersed AuNPs supported on Al₂O₃ exhibit high activity toward FA dehydrogenation. Au also exhibits a catalytic activity in the Water Gas Shift (WGS) reaction. Thanks to WGS, CO levels can be minimized by the same gold catalyst by its in situ conversion to H₂ and CO₂. Overall, AuNPs are promising catalysts for this reaction. As reported by Bi et al. [34], the formic acid / triethylamine (FA/NEt₃) adduct decomposition is a suitable model reaction to investigate the catalytic activity and stability of nanomaterials. NEt₃ is usually employed as co-catalyst to improve the reaction yield since it forms a quasi-ionic adduct that promotes the dehydrogenation process [45]. NAs, mcNAs, and scNAs catalytic activity has been evaluated on FA/NEt₃ adduct by employing the "water displacement method" (Fig. 3A). This experimental approach is appropriate for reaction in which low water soluble gas mixtures are generated [46].

In Fig. 3B and Fig. S5 the FA catalytic decomposition performances of NAs, mcNAs and scNAs are reported. Catalysts are dispersed in FA/NEt₃ pure adduct (FA / NEt₃ 1:1 mol ratio) and tested at 60 °C, monitoring the evolved gas as a function of reaction time. From the kinetic data, all the tested catalysts exhibit an improved gas evolution respect to the control. Usually, the catalytic performance of nanomaterials decreases dramatically with the S/V ratio [6]. In this case, the reaction rate decrease is relatively mild for mcNAs and scNAs. Ideally, a partially or totally bare catalyst, respectively mcNAs and scNAs, tends to expose the maximum number of active sites on the catalyst surface [47]. Thus, the two opposite effects are buffered and both the mcNAs and scNAs still maintain some catalytic features.

TEM imaging has been performed in order to investigate potential structural alterations induced by the catalytic tests (Fig. 3C). Frequently, catalysts experience morphological modifications as sintering, which negatively affect the catalytic activity and recycling [48, 49]. On this hand, NAs are designed to avoid these effects and improve recyclability and stability [50]. In particular, the hollow silica capsules efficiently protect the core catalyst from coalescence phenomena by simply acting as a physical shield [7]. NAs, mcNAs, and scNAs do not display significant morphologic changes after the catalytic tests. In particular, no gold leakage nor NAs shell damage have been observed. Evidences connected with sintering phenomena, such as coalescence and Ostwald ripening, are not found. This evidence confirms that the silica shell can improve the lifetime of the catalyst in this reaction conditions.







Fig. 3 a Experimental setup used for the FA/NEt₃ adduct catalytic decomposition. As reactor, a Schlenk tube (1) mounted on a stirrer/ thermal heater was used (2). Evolved gasses in the Schlenk reach by a tube (3) the volume measurement apparatus (4), which is an upside down 25 mL burette filled with oversaturated salt solution. The gas mixture, which escapes from the reactor, reaches the burette and displaces the solution column for a volume equal to the reaction evolved gas. **b**

Reaction rate of NAs, *mc*NAs, and *sc*NAs. In red the samples, and in green, as control, the reaction rate of the pure FA/NEt₃ adduct decomposition. Reaction conditions: 5 mg of catalyst is tested with 1.2 mL scale of FA/NEt₃ pure adducts (1:1 mol ratio) at 60 °C. **c** Post catalysis NAs TEM morphologic investigation. Left, center and right are TEM bright field images of NAs, *mc*NAs and *sc*NAs, respectively. Scale bars 200 nm

3 Conclusions

In summary, we have demonstrated the controlled composition of a family of versatile nano-architectures comprising a partially or completely bare active part. Besides their comprehensive characterizations, we compared their activity toward the FA decomposition for the in situ generation of hydrogen. Interestingly, we recognized a decrease in the catalytic activity as a function of the annealing temperature, that is associated to the equilibrium between the size-increase of the active part and the barer catalytic surface, confirming the rationally design of nanocatalysts is an essential pre-requisite.



4 Materials and methods

4.1 Nanoarchitectures (NAs) production

The following protocol was standardized for the production of 1.5 mg NAs in about 4 h. The protocol can be scaled-up to 15 mg [18].

4.1.1 Gold nanoarchitecture

Synthesis of Ultrasmall gold nanoparticles In a rounded flask with 20 mL of milliQ water, 10 μ L of 30% PSS (poly(sodium

4-styrene sulfonate)) solution are added during vigorous stirring. 200 μ L of 10 mg/mL HAuCl₄ (tetra chloroauric acid) are added to the solution pot. In a single fast shot, 200 μ L of 8 mg/mL NaBH₄ (sodium borohydride) solution are added. The solution turns instantly from bright yellow to dark red/brown and in 10 min it becomes a brilliant red.

Synthesis of gold nanoparticles arrays At very low stirring rate, 75 μ L of 40 mg/mL PLL (poly-L-lysine) solution are added. After 20 min of gentle stirring, the solution is centrifuged at 14000 rpm for 3 min. The supernatant is discarded and 2 mL of milliQ water is added to the centrifuge tube to resuspend the precipitate helped by a gentle sonication. All the precipitate that did not resuspend is discarded.

Synthesis of NAs The 2 mL nanoarrays solution is divided in two tubes, 1 mL each, to perform the Stöber reaction where silica shell is formed. In each tube, 35 mL of EtOH (ethanol) is mixed with 1.2 mL of 30% NH₄OH (ammonia solution) and 20 μ L of TEOS (tetraethyl orthosilicate).

These tubes are closed and gently shaken for 3 h on a tilting plate. The tubes are centrifuged for 30 min at 4000 rpm to discard the supernatant. The precipitated NAs are resuspended in 4 mL of EtOH by sonication and they are washed two times in EtOH. After a short spin centrifugation of 15 s (reaching 14 k rpm), NAs bigger than about 150 nm precipitate, and the supernatant contains monodisperse NAs. The supernatant collected particles are freeze-dried overnight. Usually, about 1.5 mg of a brilliant red powder is obtained from one-shot synthesis. The product remains stable for 1 year stored in the dark at 10 °C [14]. This synthetic protocol can be scaled up to 10X reactant quantities to obtain up to 15 mg of NAs with a single synthesis.

4.2 Multicore (mcNAs) and singlecore (scNAs) nanoarchitectures production

Freeze dried NAs are transferred in a crucible pot for high temperature and annealed in a standard furnace following the reported sequence:

For mcNAs, in 15 min the temperature of 350 °C is reached and kept constant for 6 h.

For *sc*NAs, in 15 min the temperature of 200 °C is reached and kept constant. At 135 min, the temperature is raised up to 400 °C in 15 min. Reached 400 °C, the heating rate is set to 100 °C h⁻¹ and maintained for 2 h. Reached 600 °C, the temperature is maintained constant for 105 min.

It is recommended to wait the cool down of the furnace before removing the samples. The resulting powder undergoes a color change turning black for *mc* and shiny pink for *sc*NAs. Samples are recovered from the crucible by dispersing it in 1 mL of EtOH.

4.2.1 Transmission Electron microscopy (TEM)

TEM observations of nanoparticles are carried out on a ZEISS Libra 120 TEM operating at an accelerating voltage of 120 kV, equipped with an in-column omega filter to perform energy filtered imaging and EELS analysis. The colloidal solutions are deposited on 300-mesh carbon-coated copper grids and observed after at least 5 h from the deposition.

4.2.2 FT-IR spectroscopy

Infrared spectra are recorded using a Diamond ATR sampling block for a Cary 630 FTIR (Agilent Technologies, Santa Clara, CA, USA). The spectra of polymers are obtained from around 10 μ L of liquid samples (50% in water). NAs spectra are recorded with around 100 μ g of freeze-dried samples.

4.2.3 ICP-MS analyses

Nanoparticles are dissolved in 1 mL ICP-MS grade HNO₃ and digested by microwave irradiation (200 $^{\circ}$ C/15 min) in borosilicate glass vessels. The resulting solution is diluted to 10 mL with ICP-MS grade water, and content of gold was determined by ICP-MS analysis against a standard calibration curve.

4.2.4 PXRD analyses

NAs are characterized through powder XRD by recording their patterns on a STOE Stadi P x-ray powder diffractometer working in Debye-Scherrer geometry equipped with Cu-K_{α 1} radiation (λ = 1.5406 Å), a Ge (111) Johansson monochromator and a MYTHEN2 1 K detector from Dectris. The XRD patterns have been collected in a 2 θ range of 10–95°, with a step of 0.03° and a time/step of 6 s. Samples are gently grounded into a fine powder with pestle and mortar and transferred in a 0.8 mm silica capillary, which is placed on the diffraction holders.

4.3 Catalytic tests

Liquid-phase formic acid decomposition is conducted in a 5 mL Schlenk reactor. The reactor is placed in a paraffin oil bath and a heater/magnetic stirrer is sets at 1.1 k rpm of stirring rate and a temperature of 60 °C. The Schlenk reactor is connected to a displacement volume meter thanks to a tube. The typical experimental procedure was the following. 5 mg of dried nano-architectures (around 400 μ g in gold) are dispersed in 0.5 mL of pure FA helped by a gentle sonication. The adduct FA/NEt₃ is formed (FA / NEt₃ 1:1 mol ratio) and transferred in the Schlenk reactor, which is already thermoset at 60 °C, during high stirring rate. The gas evolution is monitored in an upside down 25 mL burette filled with



oversaturated salt solution. This method is also called water displacement method. Experimental data, which are curves of evolved gas volume (mL) vs time (min), are obtained by a single test, linearly fitted and intercept corrected to extract the rate slope expressed in mL of evolved gas versus time (mL/min).

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Compliance with ethical standards

Conflict of interest The authors declare no conflict of interest.

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