

Faculty of Mechanical Engineering



Master of Science in Mechanical Engineering

2022

INVESTIGATION OF ONE-DIRECTIONAL AND BI-DIRECTIONAL FLOWS ACROSS STAGGERED TUBE BANKS HEAT EXCHANGER

NURJANNAH BINTI HASBULLAH



INVER Faculty of Mechanical Engineering

UNIVERSITI TEKNIKAL MALAYSIA MELAKA

DECLARATION

I declare that this thesis entitled "Investigation of One-directional and Bi-directional Flows across Staggered Tube Banks Heat Exchanger" is the result of my own research except as cited in the references. The thesis has not been accepted for any degree and is not concurrently submitted in candidature of any other degree.



APPROVAL

I hereby declare that I have read this thesis and in my own opinion this thesis is sufficient in terms of scope and quality for the award of Master of Science in Mechanical Engineering.

Signature Supervisor's Name : Dr. Fatimah Al-Zahrah binti Mohd Sa'at 14/6/2022 Date اوىيۇ **UNIVERSITI TEKNIKAL MALAYSIA MELAKA**

DEDICATION

I dedicate this thesis to my dearest parents and also my family, who have been my source of inspiration and gave me strength when I thought of giving up, who continually provide their moral, spiritual, emotional and financial supports.



ABSTRACT

One-directional and bi-directional flow conditions are different in terms of the direction of fluid flows. One-directional flow condition is when the fluid flows only in one direction. Meanwhile, bi-directional flow condition happens when the fluid flows in back and forth directions and this has been found in applications such as thermoacoustics. Thermoacoustics offer green technology for refrigeration and power cycles. The technology is appealing, but the lack of understanding on fluid dynamics and heat transfer behaviours of flow inside the system lead to the ambiguous use of equations from the wellknown one-directional flow during the design stage and the impact of such estimation becomes evident as the flow in the real system becomes more complex. For this reason, experimental investigations that are supplemented by computational fluid dynamics modelling results are carried out with a focus on the heat exchanger. A staggered tubebanks heat exchanger was tested. A thermoacoustic's standing wave rig with different type of flow inducers is used to create the one-directional and the bi-directional flows for the experiments. Results of velocity and temperature were recorded at the upstream and downstream locations of the staggered tube banks heat exchanger. The frequency of the bidirectional flow was set based on the resonance frequency of 14.2 Hz. Results indicate that temperature and velocity changes with respect to the change of flow amplitude are different between the one-directional and bi-directional flow conditions and the differences are in the range of 77 percent and 59.5 percent, respectively. A two-dimensional model of staggered tube banks heat exchanger is solved using a commercial software Ansys Fluent 16.0. The flow conditions were solved for the range of Reynolds between 270 and 1700 using SST k-w turbulence models and the temperature contour, vorticity contour and the velocity vectors were discussed based on the results of the validated models. A similar trend of Nusselt number changes with the change of Reynolds number is seen between the experimental and numerical works of the one-directional flow and the bi-directional flow conditions, with errors of amplitude expected to be due to the limitations of experimental apparatus as well as the simplifications and assumptions made for the computational fluid dynamics works. Nevertheless, most recorded differences fell within the experimental uncertainty values of \pm 2.8 to \pm 5.8. The computational fluid dynamics models provided insight into the visualization of flow in area that could not be seen experimentally. Evidently, the bi-directional flow conditions are different compared to the one-directional flow condition by 65.85 percent at Reynolds number of 1300. Therefore, the use of the well-established one-directional flow equation on bi-directional flow conditions should be avoided should an accurate result is needed in the design stage of the future thermoacoustic energy systems.

KAJIAN ALIRAN SATU-ARAH DAN DUA-ARAH MERENTASI BANK TIUB TIDAK SERENTAK PENUKAR HABA

ABSTRAK

Keadaan aliran satu arah dan dua arah adalah berbeza dari segi arah aliran bendalir. Keadaan aliran satu arah berlaku apabila bendalir mengalir dalam satu arah. Sementara keadaan aliran dwi-arah berlaku apabila bendalir mengalir ke hadapan dan ke belakang dalam dua arah dan telah ditemui dalam aplikasi seperti termoakustik. Termoakustik menawarkan teknologi hijau untuk kitaran penyejukan dan kuasa. Teknologi ini menarik, tetapi kekurangan pemahaman tentang dinamik bendalir dan gelagat pemindahan haba di dalam sistem membawa kepada penggunaan kaedah anggaran dengan menggunaan persamaan yang terkenal daripada aliran satu arah semasa peringkat reka bentuk sistem dan kesan anggaran tersebut menjadi jelas apabila aliran dalam sistem sebenar menjadi lebih rumit. Atas sebab ini, penyiasatan ujikaji yang disokong dengan kajian pemodelan dinamik bendalir dijalankan dengan fokus pada penukar haba. Penukar haba bank tiub tidak serentak telah diuji. Alatan ujikaji termoakustik dengan gelombang berdiri serta jenis pengaruh aliran yang berbeza digunakan untuk mencipta aliran satu arah dan dua arah untuk ujikaji. Keputusan halaju dan suhu telah direkodkan di lokasi hulu dan hilir penukar haba bank tiub tidak serentak. Kekerapan aliran dua arah ditetapkan berdasarkan frekuensi salunan 14.2 Hz. Keputusan menunjukkan bahawa perubahan suhu dan halaju dengan peningkatan amplitud aliran satu arah dan dua arah adalah berbeza dan perbezaannya adalah masing-masing pada julat 77 peratus dan 59.5 peratus. Model dua dimensi penukar haba bank tiub tidak serentak dibangunkan dalam perisian komersial Ansys Fluent 16.0. Keadaan aliran telah diselesaikan untuk julat nombor Reynolds di antara 270 dan 1700 dengan menggunakan model SST k- ω dan kontur suhu, kontur vorteks dan vektor halaju telah dibincangkan berdasarkan keputusan model yang telah disahkan. Corak perubahan nombor Nusselt berdasarkan perubahan nombor Reynolds dari ujikaji dan model simulasi adalah sama dengan ralat yang dijangka disebabkan oleh batasan radas ujikaji serta pemudahan, dan andaian yang dibuat oleh simulasi CFD. Namun begitu, kebanyakan perbezaan yang direkodkan berada dalam nilai ketidakpastian eksperimen di antara \pm 2.8 hingga \pm 5.8. Model CFD memberikan gambaran tentang aliran di kawasan yang tidak dapat dilihat secara eksperimen. Jelas sekali, keadaan aliran dua arah adalah berbeza berbanding dengan keadaan aliran satu arah dengan 65.84 peratus pada nombor Reynolds 1300. Oleh itu, penggunaan persamaan mantap dari aliran satu arah di dalam analisis aliran dua arah harus dielakkan sekiranya keputusan yang tepat diperlukan dalam peringkat reka bentuk sistem tenaga termoakustik pada masa hadapan.

ACKNOWLEDGEMENT

First and foremost, I would like to express my heartfelt gratitude to my supervisor, Senior Lecturer Dr. Fatimah Al-Zahrah binti Mohd Sa'at of the Faculty of Mechanical Engineering, Universiti Teknikal Malaysia Melaka (UTeM), for her invaluable guidance, support, and encouragement in completing this thesis.

I would also want to thank Senior Lecturer Dr. Mohamad Firdaus bin Sukri from the Faculty of Mechanical Engineering, Universiti Teknikal Malaysia Melaka, who is a co-supervisor of this research, for his advice and ideas in improving this study.

Special thanks to Universiti Teknikal Malaysia Melaka (UTeM) for providing the opportunity for conducting research for this study and special appreciation goes to Kementerian Pengajian Tinggi Malaysia for the financial support through the RACER/2019/FKM-CaRE/F00407 grant funding.

I also want to thank Mr. Faizal bin Jaafar, an assistant engineer at the Advanced Fluid Mechanics Laboratory, for his support and efforts in the laboratory. Special thanks to all of my peers, my dear mother, and my sister and brothers for their unwavering support and understanding while I work on my thesis. Finally, I would like to thank everyone who was there at critical stages of our project.

TABLE OF CONTENT

CHAPTER 1. INTRODUCTION 1.1 Background of study 1.2 Problem statement 1.3 Objectives of study 1.4 Scopes of study 1.5 Thesis structures 2. LITERATURE REVIEW 2.1 Overview 2.2 Tube banks heat exchanger 2.3 Fluid flow behaviour 2.3.1 One-directional flow condition 2.3.2 Bi-directional flow condition 2.3.1 One-directional flow condition 2.4.1 Basic components of thermoacoustics system 2.4.2 Standing wave and travelling wave 2.5 Heat transfer 2.5.1 Heat transfer in one-directional flow condition 2.5.2 Heat transfer in bi-directional flow condition					
1. INTRODUCTION 1 1.1 Background of study 1 1.2 Problem statement 5 1.3 Objectives of study 6 1.4 Scopes of study 7 1.5 Thesis structures 8 2. LITERATURE REVIEW 10 2.1 Overview 10 2.3 Fluid flow behaviour 13 2.3.1 One-directional flow condition 15 2.3.2 Bi-directional flow condition 17 2.4.1 Basic components of thermoacoustics system 24 2.4.2 Standing wave and travelling wave 26 2.5 Heat transfer 28 2.5.1 Heat transfer in one-directional flow condition 31 2.5.2 Heat transfer in bi-directional flow condition 31 2.5.2 Heat transfer in bi-directional flow condition 31 2.5.2 Heat transfer in bi-directional flow condition 32					
1.1 Background of study 1 1.2 Problem statement 5 1.3 Objectives of study 6 1.4 Scopes of study 7 1.5 Thesis structures 8 2. LITERATURE REVIEW 10 2.1 Overview 10 2.3 Fluid flow behaviour 13 2.3.1 One-directional flow condition 15 2.3.2 Bi-directional flow condition 15 2.4.1 Basic components of thermoacoustics system 24 2.4.2 Standing wave and travelling wave 26 2.5 Heat transfer 28 2.5.1 Heat transfer in one-directional flow condition 31 2.5.2 Heat transfer in bi-directional flow condition 32					
1.2 Problem statement 5 1.3 Objectives of study 6 1.4 Scopes of study 7 1.5 Thesis structures 8 2. LITERATURE REVIEW 10 2.1 Overview 10 2.2 Tube banks heat exchanger 10 2.3 Fluid flow behaviour 13 2.3.1 One-directional flow condition 15 2.3.2 Bi-directional flow condition 17 2.4 Thermoacoustics system 22 2.4.1 Basic components of thermoacoustics system 24 2.4.2 Standing wave and travelling wave 26 2.5 Heat transfer 28 2.5.1 Heat transfer in one-directional flow condition 31 2.5.2 Heat transfer in bi-directional flow condition 31 2.5.2 Heat transfer in bi-directional flow condition 32					
1.3 Objectives of study 6 1.4 Scopes of study 7 1.5 Thesis structures 8 2. LITERATURE REVIEW 10 2.1 Overview 10 2.2 Tube banks heat exchanger 10 2.3 Fluid flow behaviour 13 2.3.1 One-directional flow condition 15 2.3.2 Bi-directional flow condition 17 2.4 Thermoacoustics system 22 2.4.1 Basic components of thermoacoustics system 24 2.4.2 Standing wave and travelling wave 26 2.5 Heat transfer 28 2.5.1 Heat transfer in one-directional flow condition 31 2.5.2 Heat transfer in bi-directional flow condition 31 2.5.2 Heat transfer in bi-directional flow condition 31					
1.4Scopes of study 1.571.5Thesis structures82.LITERATURE REVIEW102.1Overview102.2Tube banks heat exchanger102.3Fluid flow behaviour132.3.1One-directional flow condition152.3.2Bi-directional flow condition172.4Thermoacoustics system222.4.1Basic components of thermoacoustics system242.4.2Standing wave and travelling wave262.5Heat transfer282.5.1Heat transfer in one-directional flow condition312.5.2Heat transfer in bi-directional flow condition32					
1.5 Thesis structures 8 2. LITERATURE REVIEW 10 2.1 Overview 10 2.2 Tube banks heat exchanger 10 2.3 Fluid flow behaviour 13 2.3.1 One-directional flow condition 15 2.3.2 Bi-directional flow condition 15 2.4 Thermoacoustics system 22 2.4.1 Basic components of thermoacoustics system 24 2.4.2 Standing wave and travelling wave 26 2.5 Heat transfer 28 2.5.1 Heat transfer in one-directional flow condition 31 2.5.2 Heat transfer in bi-directional flow condition 31 2.5.2 Heat transfer in bi-directional flow condition 31					
2. LITERATURE REVIEW 10 2.1 Overview 10 2.2 Tube banks heat exchanger 10 2.3 Fluid flow behaviour 13 2.3.1 One-directional flow condition 15 2.3.2 Bi-directional flow condition 17 2.4 Thermoacoustics system 22 2.4.1 Basic components of thermoacoustics system 24 2.4.2 Standing wave and travelling wave 26 2.5 Heat transfer 28 2.5.1 Heat transfer in one-directional flow condition 31 2.5.2 Heat transfer in bi-directional flow condition 31					
2.6Numerical investigations on bi-directional flow condition362.7Uncertainty studies on experimental investigations39					
METHODOLOGY 41					
3.1 Overview 41					
3.2 Experimental setup 42					
3.2.1 Flow inducers 43					
3.2.2 Test section 47					
3.2.3 Heater 49					

		3.2.4 Measuring equipment	51			
	3.3	Computational fluid dynamics model development	53			
		3.3.1 Grid independency test	56			
		3.3.2 Setup for one-directional flow condition	58			
		3.3.3 Setup for bi-directional flow condition	60			
		3.3.4 Solving and visualization	62			
	3.4	Uncertainty calculation for experimental works	63			
	3.5	Summary	65			
4.	RES	ULTS AND DISCUSSIONS	66			
	4.1	Overview	66			
	4.2	Experimental results	66			
		4.2.1 Resonance frequency	66			
		4.2.2 Calibration of flow using two different flow inducers	67			
		4.2.3 Temperature changes of flow across heater	70			
		4.2.4 Velocity changes of flow across heater	74			
	4.3	Model validation	78			
	4.4	Computational fluid dynamics results	81			
		4.4.1 Temperature contour	81			
		4.4.2 Vorticity contour	91			
		4.4.1 Velocity vector	98			
	4.5	Heat transfer comparison of one-directional and bi-directional	105			
		flow conditions				
5.	CON	CONCLUSION AND RECOMMENDATIONS				
	5.1	Conclusion	109			
	5.2	Recommendations for future research	111			
		SNA LA Si Ci in int				
REF	EREN	CES CES	113			
APP	ENDIX	K A	134			
APP	ENDIX	K BJNIVERSITI TEKNIKAL MALAYSIA MELAKA	135			

LIST OF TABLES

TABLE	TITLE	PAGE
2.1	Thermal conductivities of materials at room temperature (Cengel and Ghajar, 2015)	29
2.2	Typical values of convection heat transfer coefficient (Cengel and Ghajar, 2015)	31
3.1	Model and specification of every equipment that is used in the experiment	53
3.2	Dimension of the sketch	54
3.3	Material properties of fluid and aluminium	55
3.4	Boundary conditions for one-directional model	58
3.5	Velocity and Reynolds number of one-directional flow condition	59
3.6	Drive ratio (DR) for bi-directional flow condition	60

UNIVERSITI TEKNIKAL MALAYSIA MELAKA

LIST OF FIGURES

FIGURE	TITLE	PAGE		
1.1	Schematic diagram of fluid direction in (a) bi-directional flow and (b) unidirectional flow			
1.2	Simple schematic diagram of thermoacoustic systems	4		
2.1	Tube banks staggered arrangements (Hasbullah et al., 2021)	12		
2.2	Tube banks arrangements (a) in-line arrangement and (b) staggered arrangement (Date, 2005)			
2.3	Cross flow fluid arrangement (a) both fluids unmixed and (b) one fluid mixed, one fluid unmixed (Panchal, 2018)			
2.4	One-directional fluid flows (Hasbullah et al., 2021)	16		
2.5	Bi-directional fluid flows (Hasbullah et al., 2021)	17		
2.6	Velocity profiles for different Womersly number (Feldman and Wagner, 2012)	19		
2.7	(a) Location within the parallel-plate, (b) velocity profiles of each location for low drive ratio and (c) velocity profiles of each location for high drive ratio (Allafi et al. 2020)	22		
28	Schematic diagram of thermoacoustic system (Alamir 2020)	25		
2.9	Illustration of (a) standing wave and (b) travelling wave in	23 27		
	thermoacoustics system (Saat, 2013)			
2.10	Vorticity contour at the end of stack (Berson et al., 2008)	28		
2.11	Visualisation of vortex contour at different frequencies; (a) 13.1 Hz and (b) 23.1 Hz (Saat et al., 2019)	37		
2.12	Vorticity contour for the flow at the end of the stack	38		
3.1	Flowchart of methodology	42		
3.2	Schematic diagram of the experimental setup	43		
3.3	(a) Schematic diagram and (b) real diagram of the loudspeaker	45		
3.4	Voltage regulator and amplifier	45		
3.5	(a) Schematic diagram and (b) real diagram of the blower	46		
3.6	Test section of the resonator	47		

3.7	(a) Tube banks heat exchanger and (b) enlarge view of the tube	48			
20	bank's measurement	50			
3.8	(a) Schematic diagram of heater tubes connection, (b) heater tubes and (c) heater tubes that are inserted into tube banks	30			
	through the back side of the test section				
3.0	Pressure sensor is mounted on the hard and of the rig	51			
3.9	Moscuring, acquinment used in experiment	52			
3.10 2.11	Skotch of 2D staggered tube banks	54			
3.11	Grid independency test	56			
3.12	(a) Enlarge view of mesh generation near the tube banks (b)	50			
5.15	Mesh generation of whole computational domain	57			
3 14	Propagation of error for Nusselt number. Nu	64			
<i>J</i> .1 т Л 1	Resonance frequency	67			
ч.1 Л 2	Velocity changes at inlet and outlet locations of the test section	69			
7.2	as (a) frequency of the blower increases (b) peak-to-peak	07			
	voltage input of the loudspeaker increases				
43	Temperature changes with inlet velocity in one-directional flow	71			
1.5	condition and a heated tube surface temperature of (a) 40° C	/1			
	(b) 60° C and (c) 80° C				
4.4	Temperature changes with inlet velocity in bi-directional flow	73			
	condition and a heated tube surface temperature of (a) 40° C, (b)				
	60°C and (c) 80°C				
4.5	Velocity changes with flow amplitude in one-directional flow	76			
	condition and a heated tube surface temperature of (a) 40° C, (b)				
	60°C and (c) 80°C				
4.6	Velocity changes with flow amplitude in bi-directional flow	77			
	condition and a heated tube surface temperature of (a) 40°C (b)				
	60°C and (c) 80°C				
4.7	CFD model validation for cases with (a) $T_s = 40^{\circ}$ C. (b) $T_s =$	79			
	60° C and (c) $T_{s} = 80^{\circ}$ C				
4.8	Temperature contour of one-directional flow conditions at $T_s =$	82			
	40°C	-			
4.9	Temperature contour for bi-directional flow of (a) $DR = 0.45\%$	83			
	and (b) DR = 1.12% at $T_s = 40^{\circ}$ C				
4.10	Temperature contour of one-directional flow at $T_s = 60^{\circ}$ C	84			
4.11	Temperature contour for bi-directional flow of (a) DR 0.48%	87			
	and (b) DR 1.63 % at $T_s = 60^{\circ}$ C				
4.12	Temperature contour of one-directional flow at $T_s = 80^{\circ}$ C	88			
4.13	Temperature contour for bi-directional flow of (a) $DR = 0.49$ %	90			
	and (b) DR 1.64 % at $T_s = 80^{\circ}$ C				
4.14	Vorticity contour for one-directional flow at $T_s = 40^{\circ}$ C	91			

4.15	Vorticity contour for bi-directional flow of (a) $DR = 0.45$ % and	92
	(b) DR = 1.12 % at $T_s = 40^{\circ}$ C	
4.16	Vorticity contour of one-directional flow at $T_s = 60^{\circ}$ C	93
4.17	(a) Vorticity contour for bi-directional flow of (a) $DR = 0.48$ %	95
	and (b) DR = 1.63 % at $T_s = 60^{\circ}$ C	
4.18	Vorticity contour of one-directional flow $T_s = 80^{\circ}$ C	96
4.19	Vorticity contour of bi-directional flow of (a) $DR = 0.49$ % and	97
	(b) DR = 1.64 % at $T_s = 80^{\circ}$ C	
4.20	Velocity vector of one-directional flow condition at $T_s = 40^{\circ}$ C	98
4.21	Velocity vector for bi-directional flow of (a) $DR = 0.45$ % and	100
	(b) DR = 1.12 % at $T_s = 40^{\circ}$ C	
4.22	Velocity vector of one-directional flow condition at $T_s = 60^{\circ}$ C	101
4.23	Velocity vector for one-directional flow of (a) $DR = 0.48$ % and	102
	(b) DR = 1.63 % at $T_s = 60^{\circ}$ C	
4.24	Velocity vector of one-directional flow condition at $T_s = 80^{\circ}$ C	103
4.25	Velocity vector for one-directional flow of (a) $DR = 0.49$ % and	104
	(b) DR = 1.64 % at $T_s = 80^{\circ}$ C	
4.26	Nusselt number of one-directional and bi-directional flow	107
	conditions for flow with Reynolds that ranges between 270 and	
	1700	
	اونيةم سيتر تتكنيكا مليسيا ملاك	

UNIVERSITI TEKNIKAL MALAYSIA MELAKA

LIST OF ABBREVIATIONS AND SYMBOLS

2D	-	Two-dimensional
CFC	-	Chlorofluorocarbon
CFD	-	Computational Fluid Dynamics
DR	-	Drive ratio
FE	-	Finite Element
FEA	-	Finite Element Analysis
HFC	-	Hydrofluorocarbon
HVAC	-	Heating Ventilation Air Conditioning
HX	-	Heat Exchanger
LMTD	-	Log Mean Temperature Difference
NTU		Number of Heat Transfer Unit
PIV	-	Particle Image Velocimetry LAYSIA MELAKA
SST	-	Shear Stress Transport
UDF	-	User Defined Function
λ	-	Wavelength
С	-	Speed of sound
f	-	Frequency
S_L	-	Horizontal length
S_T	-	Transverse length
S_D	-	Diagonal length
D	-	Diameter of tubes
V_{in}	-	Inlet velocity
Vout	-	Outlet velocity

T _{in}	-	Inlet temperature
Tout	-	Outlet temperature
T_s	-	Surface temperature
T_o	-	Mean temperature
Pair	-	Density of air
Cp_{air}	-	Specific heat capacity
λ_t	-	Thermal conductivity
μ_{air}	-	Dynamic viscosity
α	-	Diffusivity
y^+	-	Location of the nearest node from the wall
Re	-	Reynolds number
Nu	-	Nusselt number
Pr	-	Prandtl number
Z	-	Tidal displacement
Wo		Womersly number
Lc		Characteristic length
R	-	Tube radius
υ	-	Kinematic viscosity
ω	-	Angular frequency
Umax	-	Maximum velocity amplitude
<i>x</i> ₁	-	UNIV Inlet location NIKAL MALAYSIA MELAKA
<i>x</i> ₂	-	Outlet location
m'	-	Mass flux
Р	-	Oscillating pressure
P_a	-	Pressure amplitude
P_m	-	Mean pressure
k	-	Wave number
t	-	Time
θ	-	Phase difference
Φ	-	Phase
\bar{x}	-	Mean value
n	-	Repeated numbers

Α	-	Area
L	-	Length
W	-	Width
Ż	-	Rate of heat transfer
h	-	Heat transfer coefficient
'n	-	Mass flow rate
U	-	Uncertainty
S	-	Precision uncertainty
b	-	Systematic uncertainty
σ	-	Standard deviation



LIST OF APPENDICES

TITLE	PAGE
Uncertainty calculation	134
Certificates for calibration of measuring devices used in experimental work	135
	TITLE Uncertainty calculation Certificates for calibration of measuring devices used in experimental work



LIST OF PUBLICATIONS

Nurjannah Hasbullah, Fatimah Al-Zahrah Mohd. Saat, Fadhilah Shikh Anuar, Dahlia Johari and Mohamad Firdaus Sukri. Temperature and Velocity Changes across Tube Banks in One-directional and Bi-directional Flow Conditions. *Evergreen Joint Journal of Novel Carbon Resource Sciences & Green Asia Strategy*, Vol. 08, Issue 02, pp.428-437.

Nurjannah Hasbullah, Fatimah Al Zahrah Mohd Saat, Fadhilah Shikh Anuar, Mohamad Firdaus Sukri and Patcharin Saechan. Experimental and numerical studies of onedirectional and bi-directional flow conditions across tube banks heat exchanger. *Thermal Science Engineering Progress*, Vol. 28, pp. 101176.

Nurjannah Hasbullah, Fatimah Al Zahrah Mohd Saat, Fadhilah Shikh Anuar, Mohamad Firdaus Sukri, Zaid Akop and Zainuddin Abdul Manan (2021, November 23). *Uncertainty analysis of thermal fluid measurements for bi-directional flow condition across tube banks* [Paper presentation] ICESEAM 2021: Melaka, Malaysia.

Nurjannah Hasbullah, Fatimah Al Zahrah Mohd Saat, Fadhilah Shikh Anuar, Mohamad Firdaus Sukri, Mohd Zaid Akop, Zainuddin Abdul Manan (2021). *Experimental study on the performance of one-directional and bi-directional flow conditions across in-line tube banks heat exchanger*. Manuscript submitted for publication.



CHAPTER 1

INTRODUCTION

1.1 Background of study

Heat exchangers are devices that are used at various temperatures for the purposes of transferring heat between two or more fluid sources. Heat exchangers are commonly used in applications such as power generation, chemical processing, electronics cooling, air conditioning, refrigeration and automotive industry (Kuruneru et al., 2020). Heat exchanger is a system involving the heat exchange between two fluids with two different temperatures; the high temperature fluid usually known as a hot fluid and the low temperature fluid commonly referred as the cold fluid. The heat transfer process between the two fluids takes place in the heat exchangers (Afonso et al., 2003). The efficiency of the heat transfer process varies with the change of flow conditions and directions. Shell-and-tube heat exchanger is one of the types of heat exchangers that consist of a collection of tubes containing fluid that either be heated or refrigerated (Raju et al., 2014). The other fluid runs over the heated or cooled pipe, so that it can either supply the heat or absorb the heat. A package of tubes is called a bundle of tubes and may consist of many types of tubes, such as regular and longitudinally finished. Typically, the heat exchangers for shells and tubes are used for high pressure applications. This is because the heat exchangers that consist the shell and the tube are robust because of their shape (T'Joen et al., 2009). In addition to the shape and dimension of the heat exchanger, the direction of fluid flow also plays role on the rate of heat transfer between the fluids. In most situations, the fluid flows in one direction only. Nonetheless, in some cases, the fluid flows not in the normal steady onedirectional form but in different directions such as the flow of blood, oscillatory flow in thermoacoustic engine or cooler and the flow in an ocean (Yang et al., 2017). The oscillatory flow of blood flow, thermoacoustic energy system and the ocean flow can be defined as a bi-directional flow as the fluid flows forth and back in two main directions. Nevertheless, it is found that the basic understanding of heat transfer in flows other than steady one-directional flow condition is uncommon. Investigation is needed and this requires comprehensive methods which will be able to reveal differences or similarity of behaviours between the two different type of flow conditions; the bi-directional flow condition and the usual one-directional condition.

The bi-directional flow condition can be found in the relatively new green technology known as thermoacoustic technology. The technology can be used for power cycle as well as refrigeration cycle. In this modern world, refrigeration plays a central role as it is needed in almost all aspects of technology (Wang et al., 2018). The process of cooling occurs through the process of compression of vapour, which uses a specific coolant. After its introduction in the early 19th century, the refrigeration system underwent much developments. Nevertheless, the traditional refrigeration device poses a significant threat to the atmosphere through the production of green-house gases that deplete ozone (Hunt and Raman, 2017). To achieve the appropriate temperature, blends of carbon, hydrogen, fluorine, and chlorine are mixed in different ratios. This also has the potential to cause global warming. In addition, the vapour compression system entails high cost of electricity. After determining these harmful impacts, efforts are made to start moving over from standard refrigeration on an ongoing basis. In general, resources must be efficiently utilized, which may be accomplished, among other things, by several technological advancements (World Energy Council, 2018). Thermoacoustic technology is one developing technology

with this potential. This technique may be used with sound waves and heat as inputs inside a pressured environment to generate either power (engine) or cooling effect (refrigerator). This system also has a number of advantages, such as the fact that it operates without moving parts and uses non-harmful chemicals as a working fluid, making it a potentially appealing technology. Thermoacoustic cooling is a viable substitute, as it offers the preferred cooling level without the need for any harmful substances (Leclaire and Heldebrant, 2018). The bi-directional flow conditions of thermoacoustics is less understood (Hasbullah et al., 2021). Figure 1.1 shows the comparison of fluid direction between the oscillatory flow of thermoacoustics, or also known as bi-directional flow, and the unidirectional flow that has been widely used in many conventional systems. Bi-directional flow is a condition where the fluid flows back and forth in the system while in unidirectional flow the fluid flows only in one direction.



Figure 1.1: Schematic diagram of fluid direction in (a) bi-directional flow and (b) unidirectional flow

Since technological development must focus not only on the performance of the system but also on the technological impact on the environment, thermoacoustics which provide green technology for at least two major applications; cooling and power generation equipment, are favourable. Figure 1.2 shows a simple thermoacoustic mechanism.

Basically, the thermoacoustic system consists of a loudspeaker as an acoustic driver, a tube banks heat exchanger and a resonator as the main body of the system. In thermoacoustics, the heat exchangers as well as the stack/regenerator that are used in the system are also referred to as porous media due to the feature of porous structure with micro and mini sizes pores (Saat, 2013). A more complicated arrangements can be used to obtain better efficiency but the simple mechanism, as shown in Figure 1.2, should be sufficient to create the thermoacoustic environment.



The acoustic wave contains variations of pressure and volume flow rate that oscillates depending on the frequency of the flow. The proper phasing between the acoustically induced fluid displacement and its compression or expansion, combined with heat transfer process would result in the application of Stirling-like thermodynamic cycles which are of engineering problems significance. The use of harmless refrigerants such as hydrogen, helium or some other inert gas as a working medium is environmentally friendly and provide benefits to the technology. The thermoacoustic cooling system provides additional advantages of lower operating costs because there are no moving parts and thus there is no lubrication system requirement. Due to the promising feature of thermoacoustic technology, the oscillatory flow condition of thermoacoustics has been selected to represent