

University of North Dakota [UND Scholarly Commons](https://commons.und.edu/)

[Theses and Dissertations](https://commons.und.edu/theses) [Theses, Dissertations, and Senior Projects](https://commons.und.edu/etds)

January 2023

Studying Phase And Morphology Of Hydrocarbon Petrochemicals In Inorganic And Organic Microdroplets Using An Electrodynamic Balance

Fafa Tackie-Otoo

How does access to this work benefit you? Let us know!

Follow this and additional works at: [https://commons.und.edu/theses](https://commons.und.edu/theses?utm_source=commons.und.edu%2Ftheses%2F5271&utm_medium=PDF&utm_campaign=PDFCoverPages)

Recommended Citation

Tackie-Otoo, Fafa, "Studying Phase And Morphology Of Hydrocarbon Petrochemicals In Inorganic And Organic Microdroplets Using An Electrodynamic Balance" (2023). Theses and Dissertations. 5271. [https://commons.und.edu/theses/5271](https://commons.und.edu/theses/5271?utm_source=commons.und.edu%2Ftheses%2F5271&utm_medium=PDF&utm_campaign=PDFCoverPages)

This Thesis is brought to you for free and open access by the Theses, Dissertations, and Senior Projects at UND Scholarly Commons. It has been accepted for inclusion in Theses and Dissertations by an authorized administrator of UND Scholarly Commons. For more information, please contact und.commons@library.und.edu.

STUDYING PHASE AND MORPHOLOGY OF HYDROCARBON PETROCHEMICALS IN INORGANIC AND ORGANIC MICRODROPLETS USING AN ELECTRODYNAMIC BALANCE

by

Fafa Tackie-Otoo Bachelor of Science Mechanical Engineering, Kwame Nkrumah University of Science and Technology, 2016

A Thesis

Submitted to the Graduate Faculty

of the

University of North Dakota

In partial fulfillment of the requirements

for the degree of

Master of Science

Mechanical Engineering

Grand Forks, North Dakota

May

2023

Name: Fafa Tackie-Otoo

Degree: Master of Science

This document, submitted in partial fulfillment of the requirements for the degree from the University of North Dakota, has been read by the Faculty Advisory Committee under whom the work has been done and is hereby approved.

This document is being submitted by the appointed advisory committee as having met all the requirements of the School of Graduate Studies at the University of North Dakota and is hereby approved.

-DocuSigned by: Clins Mison -2E0AF088C733403

Chris Nelson Dean of the School of Graduate Studies 5/4/2023

Date

PERMISSION

Title Studying Phase and Morphology of Hydrocarbon Petrochemicals in Inorganic and

Organic Microdroplets Using an Electrodynamic Balance

Department Mechanical Engineering

Degree Master of Science

In presenting this thesis in partial fulfillment of the requirements for a graduate degree from the University of North Dakota, I agree that the library of this University shall make it freely available for inspection. I further agree that permission for extensive copying for scholarly purposes may be granted by the professor who supervised my thesis work or, in his absence, by the Chairperson of the department or the dean of the School of Graduate Studies. It is understood that any copying or publication or other use of this thesis or part thereof for financial gain shall not be allowed without my written permission. It is also understood that due recognition shall be given to me and to the University of North Dakota in any scholarly use which may be made of any material in my thesis.

> Fafa Tackie-Otoo 05/04/2023

TABLE OF CONTENTS

TABLE OF FIGURES

TABLE OF TABLES

ACKNOWLEDGEMENTS

I want to sincerely thank my thesis advisor, Dr. Hallie Boyer Chelmo, for her advice and wisdom throughout my academic career at the University of North Dakota. I want to thank my thesis committee members Dr. Jeremiah Neubert and Dr. Surojit Gupta.

I want to express my gratitude to Dr. Ryan Davis for setting up the dual balance electrodynamic trap (DBET) and the MicroLev team for their support. Additionally, I would like to express my gratitude to Dr. Clement Tang and Dr. Surojit Gupta for their unwavering support during my scholarly pursuits.

I want to convey my appreciation to the North Dakota Water Resources Research Institute (NDWRRI) and University of North Dakota's College of Engineering and Mines for their guidance and support during my time in the master's program at the University of North Dakota.

I am appreciative of all the connections I was able to make on campus with both instructors and students. Without their assistance, my success would not have been feasible.

To my ever-supportive husband, Nii Otinkoran and son-to-be Nii Okai.

ABSTRACT

Wastewater from the petroleum industry contains large amounts of inorganic salts, hydrocarbons, mercaptans, oil and grease, phenols, and other organic chemicals. All these compounds can be found in highly complex solutions in the petroleum industry's discharged water, and there is no common treatment method, which precludes reuse paths in other sectors such as irrigation of farmland. In order to reuse produced water, the water must be treated and these harmful chemicals must be removed. To treat and potentially reuse oily waste outside the energy sector, researchers typically use membrane technology, photocatalytic degradation, oxidation processes, electrochemical catalysis, and other methods. The goal of this project is to introduce a novel method to measure chemical thermodynamic properties, such as water activities, of produced water. I demonstrate that the electrodynamic balance (EDB) technology is beneficial for exploring properties of produced water that can be applied to treatment and reuse in the future.

NOMENCLATURE

1.0 INTRODUCTION

1.1 Relationship between produced water (PW) and atmospheric aerosol (AA)

In this chapter, I introduce the sources and importance of produced water (PW), atmospheric aerosol (AA), and I also explain the relationship between them. First, PW is generated by the oil and gas energy sector; it is the fresh water that emerges from the well along with the crude oil during extraction. As a result, PW contains suspended solids, dissolved solids, soluble and non-soluble oil/organics, and other chemicals utilized in the production process.^{1,2}

Over the course of the well's life, the proportion of produced water to oil changes. This ratio typically exceeds three and, in some regions of the world, can even exceed twenty.³ The composition of the produced water changes with time in addition to the flow rate. From well to well, generated water has a vast range in chemical make-up.

Similarly, AA are also highly variable in their chemical composition due to complex atmospheric chemical processes that govern particle formation and growth, and individual particle properties. Similar chemical compounds are present in PW and AA, owing to the overall abundance of these compounds and their inevitable mass exchange between bulk water sources and the atmosphere, such as by evaporation of volatile and semi-volatile petrochemicals.

I draw this similarity because understanding PW can shed light on AA, and vice versa; furthermore, I explore the possibility of applying techniques that have advanced the study of AA in recent years to be of potential benefit to understanding PW. Because of the large amounts of PW generated annually by the energy sector in the United States, it is necessary to explore options for treating it for potential uses in other sectors that benefit society using scientific techniques that are typically applied to studying AA.

Despite the widespread belief that oil and water do not mix well, separating the two usually necessitates several processes. The level of produced water treatment is determined by the site's treatment needs, which are often surface water discharge, deep well injection, reinjection, or evaporation ponds.⁴ Beneficial reuse is becoming a more attractive choice as rules have tightened, disposal methods have gotten more expensive, and water is becoming scarcer. Treatment of produced water is frequently regarded as an upstream oil and gas process. Removing oil and suspended particles from water can be difficult depending on the degree of chemical and mechanical emulsification.

As of now, produced water cannot be used outside the energy sector as it can pose significant challenges including high expense of treatment, the resulting water's potential for longterm toxicity, and public acceptance.⁵ Additionally, a "one size fits all" solution is unlikely because the quantity and characteristics of the produced water change over time. The goal is to improve treatment technology by first understanding the solutions to be treated.⁶

1.2 Using Aerosol Instrumentation to Study Produced Water Microdroplets

Numerous instruments can be used to detect how aerosol particles react to variations in RH. It has been shown that the electrodynamic balance (EDB)-based particle levitation approach is an effective way to examine the hygroscopic characteristics of individual aerosol particles. ⁷ This method has the benefit of enabling continuous monitoring of the particle mass as a function of RH, allowing for in situ unambiguous characterization of the particle mass growth due to water uptake. Particles with sizes greater than a few micrometers can use it. The hygroscopicity tandem differential mobility analyzer (HTDMA) is an alternative technique for measuring water uptake.⁸

In this work, I harness EDB technology to investigate using a Dual Balance Electrodynamic Trap (DBET) to measure phase transitions of briney aqueous droplets relevant to the energy sector. The key advantage of studying produced water in microdroplet form is that EDB instruments and other microparticle levitation platforms access extremely high solute concentrations known to be found in produced water. ⁹ However, the estimates of total dissolved salts (TDS) in produced water are close to supersaturation with respect to solute, which creates difficulty in using conventional methods to study produced water at these metastable concentrations. I start my tests using only binary solutions containing water and NaCl, due to the well understood chemical thermodynamics of aqueous NaCl in both bulk and droplet form, as well as the fact that NaCl is the most abundant salt in the Bakken oil and gas play in North Dakota.⁵ This project lays a foundation for near future work to accomplish exploring salt mixtures and other salt compounds, such as bromides and sulfates, as well as petrochemicals such as organic acids.

Although this thesis focuses on improving wastewater reuse in the energy sector, the mixtures I examine are also atmospherically relevant. The chemicals found in produced water are volatile or semi-volatile, and therefore partition to the atmosphere and ultimately contribute to aerosol particle loading. Therefore, it is pertinent to understand the environmental problem of how energy sector wastewater impacts amospheric aerosol. Next, I will explain the background of how atmospheric aerosols affect the environment.

1.3 Particulate Matter (PM)

In the atmosphere, aerosol particulates are referred to collectively as particulate matter (PM), which includes mineral dust, raindrops, fog, smog, smoke, soot, and haze.¹⁰ Depending on the origins, aerosol particles can be categorized as follows: direct emissions of primary particles from human or biological sources, secondary sources are created by chemical processes in the atmosphere. The primary sources of atmospheric aerosols can be divided into the following groups: (i) common surface sources of primary aerosols, such as arid soils (mineral dust), the ocean (sea salt), the biosphere (pollen), biomass (mostly OC), and fuel combustion (OC and EC); (ii) diffuse sources, such as air traffic, cloud evaporation, secondary aerosols produced by the chemical synthesis of volatile substances (organics), and extraterrestrial sources, within the atmospheric volume (vaporizing meteors), and (iii) powerful point sources, such as a volcano.¹¹

The majority of the world's aerosol emissions come from natural sources, but in urban areas, the relative anthropogenic share increases significantly. Aerosol particles have a lifespan that can run from a few hours to several days, the latter long enough to permit long-distance transport. The primary characteristic of aerosols is their variability and heterogeneity in time and space as a result of their multiple sources and comparatively brief lifetime when compared to several trace gases. Wet deposition is the primary drain. The coarse mode has significant sinks for both dry and moist deposition. Their lifetime in the stratosphere may be similar to the number of years an air parcel spends there, allowing for worldwide distribution and transit.^{10,11} The earth's radiation equilibrium is impacted by aerosol particles in the atmosphere in a variety of ways.¹²

Aerosol particles, first and foremost, absorb and disperse radiation. The hygroscopicity of the aerosol particles, which is primarily decided by their chemical composition, has an impact on this direct aerosol effect. Second, both the chemical composition and the size distribution of the aerosol particle are related to the propensity for cloud formation and the resulting cloud properties.¹³ The indirect aerosol effect is the result of this impact on cloud albedo and the radiative characteristics of cloud droplets.

Inorganic and organic components can be distinguished among atmospheric aerosols. Most inorganic salts found in the atmosphere have well-known hygroscopic characteristics. 14,15 The hygroscopic characteristics of quite a few pure substances have been studied among the numerous organic species found in the aerosol.¹⁶ However, only a small number of mixtures' hygroscopic

characteristics have been studied thus far. Inorganic salts, such as ammonium sulfate (AS) and sodium chloride, can exhibit hysteresis behavior during the uptake and loss of water, i.e., by displaying a difference between the deliquescence and efflorescence relative humidities (DRH/ERH) and with a higher water content of the deliquesced than the effloresced particles in this relative humidity (RH) range. In contrast, organic aerosol components without hysteresis behavior can help the aerosol absorb water at a lower RH than the DRH of inorganic ions. This has been documented by 17 and is also theoretically anticipated given that such complex mixtures can maintain a liquid state and exchange water with the gas phase at lower RH's.¹⁸

Organic aerosols, which are primarily produced by the photochemical oxidation of primary organic matter and volatile organic compounds (VOCs), are a significant component of fine particulate matter (PM). These aerosols have a detrimental effect on human health, air quality, and climate change.¹⁹

1.4 Organic aerosols

A significant but extremely variable portion of atmospheric aerosol is made up of organic compounds. Direct emissions of organic aerosol particulates occur from both biological sources; vegetation and the ocean, and human sources; the burning of fossil fuels, biomass, and industrial processes.20 Along with these particle emissions, there is also a gas phase emission, and the oxidation-based degradation of these precursors results in the creation of secondary organic aerosol (SOA). The anthropogenic effect is apparent in the major contribution, i.e., biomass burning. The main component of biomass-burning particles is organics.²¹ Depending on the region, aerosol particle chemical composition varies greatly.

In the haze plume from the United States, measurements over the Atlantic showed that organic aerosols dispersed at least as much light as sulfate particles. There are indications that organics occur in the lower stratosphere and are also significant components, if not the majority, of upper-tropospheric aerosols. ²² Many of the organic molecules in aerosols are water soluble due to the presence of polar functional groups, especially carboxylic and dicarboxylic acids. This influences the aerosol particles' water uptake and enables them to engage in cloud droplet nucleation 23, and 24 Recent field measurements have shown that organic aerosols may function as effective cloud nuclei and, as a result, have a significant impact on the indirect climate influence.²⁵

2.0 EXPERIMENTAL METHODOLOGY

2.1 Advantages of Using Inkjet Dispensers

Inkjet dispensers are typically used in microparticle levitation experiments due to their reliably controlled sizes of the droplets that are generated and their droplet-on-demand capability.^{29–32} Setting up operational parameters is the simplest configuration for an inkjet dispenser. It needs a controller to create the pulses, a dispenser with a reservoir and a bucket to dispense into, and an observing system (Figure 1).

An easy-to-use syringe can supply the fluid and back pressure (Some pressure control function, which for the present purpose is fairly basic, is provided by the combination of the piston of the syringe and the operator's thumb). A fixed reservoir, such as a closed vial or bottle, and a pressure system to deliver controlled back pressure to the fluid reservoir through a designated intake in the cap should be used instead of a syringe for a more serious procedure.

Figure 1: *Basic jetting setup. A second driver, not depicted in the figure, is typically used to connect the strobe LED that illuminates the droplets for the camera, MicroFab Technologies, Inc., User's Guide, June 2012, Version 4.1.*

A "Pneumatics Console" from MicroFab Technologies provides respectable manual pressure control. An Alicat controller, for which support is included into the JetServerTM application, can also be ordered. A different range of pressure control is required in some applications, such as the dispensing of fluids with high melting points; MicroFab provides a Tescom ER3000 pressure controller for this use, which is operated via a different computer interface on the same control computer. The camera will observe an almost motionless shadow of any droplet in its field of view when the strobe LED illuminating it is flashed with very brief pulses (usually approximately 10µs duration); see Figure 2.

Figure 2: *Drop formation with Sodium Chloride (NaCl).*

2.2 Product Description

My project requires dispensing microdroplets directly into an electrodynamic trap. Therefore it is worthwhile to explain the product's use in detail. MicroFab's drop-on-demand single jet dispensing devices of the MJ-A design are ideal for dispensing droplets of aqueous and solvent-based fluids at varied temperatures. Because of an integrated orifice and virtually entirely glass wetted surfaces, MJ-A devices are particularly resistant to hostile fluids. I can improve their process by selecting drop volumes within a two order of magnitude range by using orifice sizes ranging from 20 to 80 µm. Fluids with viscosities less than 20 cPs and surface tensions ranging from 20 to 70 dynes/cm can be dispensed.

The integrated orifice extends from the housing, providing visibility of both internal flow and drop creation. Metal extensions on both sides can optionally protect the orifice from injury.Microdrop dispenser heads work on the same idea as an inkjet printer with a piezoelectric print head. A capillary tube is used to feed the liquid. A piezo ceramic imparts a mechanical impulse to the liquid column to emit a droplet. A microfine droplet is formed at the nozzle tip and exits the dispenser head at high speed.The size of the drop (15-120 µm) is determined by the capillary opening and driving mode. The electronic control of the dispenser heads ensures a high level of dispensing precision in terms of volume, timing, and positioning. The operation is visible thanks to an embedded stroboscopic LED.

MJ-ABP-01

Figure 3: *Dispenser Head.*

2.2.1 Drop-on-Demand Mode (DOD)

In drop-on-demand mode, the hydrostatic pressure created by a fluid level higher than the orifice and backpressure (low vacuum) are balanced to keep the fluid meniscus at the dispenser orifice. Pressure from the piezoelectric actuator is employed to form droplets in this case. The dispensing program controls the ejection of one droplet every trigger of the device. Because the reservoir is above the orifice level, a tiny vacuum is required in drop on demand mode to prevent dripping at the orifice.

To dispense, input a waveform parameter in the software that will eject the droplet. Each fluid has a unique set of waveform parameters that are determined through an iterative process. As a starting point, create a unipolar waveform with a rise and fall time of 3.0µs, a dwell period of 30µs, a voltage of 30V, and a frequency of 240Hz.

Experimentation is used to investigate the interaction between the dispensing and catch fluids when collecting microspheres. Drop on demand microsphere dispensing is commonly accomplished by holding the dispenser tip in air over the catch solution, but I do not require this in this particular project.

2.2.2 Finding useful operating parameters

The proper operation of a jet, and its verification, is typically the first step in my experiments to ensure that the microdroplet size is in my desired range. It must be large enough to be visible in the trap. Within the range of $20 - 50$ micrometers is ideal for my experiments. The following is the standard process:

- Position the jet over a waste bucket, such that the horizontal camera can see the tip of the device and some 2 mm below it.
- Fill the jetting device.
- Ensure that the tip of the device is free of pending droplets.
- Make the device run in continuous mode and adjust pulse shape parameters until good jetting is observed.

Figure 4: *The parameter list in the main window for a controller with a choice of pulse shapes, with "arbitrary waveform" selected, MicroFab Technologies, Inc., User's Guide, June 2012, Version 4.1.*

I assume for the purpose of the ensuing step-by-step example that the JetServerTM software is already active. My objective is to outline the "mechanical" stages involved in fine-tuning a device's jetting behavior. As a result, the method for choosing specific parameters is not covered in great detail.

1. If multiple jets or dispensing channels are available, I make sure that only the one jet or channel to be worked on is showing a green device; click on its button if it is not. If then any other device icons still show green, click on each of those to make them change color to dark blue. Note that, depending on the hardware components in your setup, the number of device icons shown may vary.

- 2. I make sure the device is located over a waste bucket.
- 3. Move the jet or the horizontal camera until its tip appears in the field of view of the camera. Adjust the focus of the camera to obtain a sharp image of the tip, in particular the vertical sides of it.

Figure 5: *Jetting device tip in view of the horizontal camera for controlling jet formation during pulse shape tuning, MicroFab Technologies, Inc., User's Guide, June 2012, Version 4.1.*

Figure 5's two photos show the range of magnifications that can be used to adjust the pulse shape for jetting devices. The front faces of the devices in the image have a diameter of roughly 550μ m. Both times, it has been easier to see the device tip in the field of view using external light sources, such as a flashlight. If no readily accessible source exists, you can think about activating the main window's jetting device by pulsing it: Near the top center, click the Start Jet Continuous button; click it again to stop. This will activate the strobe light, illuminating the desired region in front of the camera (and may generate droplets already, too).

In rare instances, the camera may have a reticle projector that projects a cross with scale divisions in the middle to aid in estimating distances when calculating drop velocity. On more recent MicroFab dispensing test systems, the camera image is captured using a frame grabber and shown in a separate window on the computer screen; in this case, the display program can overlay a vertical scale.

4. In the main window, the columns of input fields on the left side include the pulse shape parameters. If you have a recommended set of numbers, type them into the corresponding fields. If you don't have any, start with the numbers shown in Figure 7, except that +20 V and -20 V are probably better dwell and echo voltages to begin with.

There are five times for "Rise 1", "Dwell", "Fall", "Echo", and "Rise 2" (also called final rise), and three voltage levels "Idle", "Dwell" and "Echo" as illustrated in Figure 6. The second half of the pulse is called the echo and needs not be used. It can be turned off by setting the echo voltage equal to the idle voltage(The total pulse length still includes the echo and final rise times).

With MicroFab's jetting devices and drive electronics, the echo part is used more often than not, the most notable exceptions being the dispensing of isopropanol and sometimes water and water-based solutions.

Figure 6: *Principle of pulse shapes used to fire jetting devices, MicroFab Technologies, Inc., User's Guide, June 2012, Version 4.1.*

5. Click on the Start Jet Continuous button. It will change to display now Stop Jetting and the jetting device will be continuously pulsed at the frequency given further down below the Stop Jetting button (Figure 7).

- 6. If the parameters are suitable for the fluid being used, formation of droplets should occur. To find out, the trigger to the strobe light needs to be delayed relative to the pulse sent to the jetting device. This can be accomplished with the slider for Strobe delay in the main window, an adjustment knob on the jet controller, or a potentiometer driven delay in the MicroFab strobe drive unit, which is either a separate box or integrated in a pneumatics console. As a rule of thumb, the drop formation at the orifice begins some time around the end of the fall in the pulse shape.
- 7. If no drop formation is present, or if it is not satisfactory, change some pulse shape parameter and press the "Enter" key. The jetting will be stopped, the changed pulse shape sent to the controller, and the jetting resumed automatically.
- 8. Another way to influence the drop formation that is useful and often required but not necessarily controlled through the JetServerTM program is the "back pressure", i.e., pressure applied to the fluid in the reservoir. This can be done with the help of a separate pneumatic console or an optional computer-operated pressure controller.

Figure 7: *Main program window with pulsing at the output going on. The trigger mode is set to continuous automatically when using the "Start Jet Continuous" button. Alternatively, the mode could be set directly in the "Trigger mode" box and the "Trigger Jet" button underneath it used to start pulsing, MicroFab Technologies, Inc., User's Guide, June 2012, Version 4.1.*

The two main purposes of changing the back pressure are as follows: The device can first be cleaned by either using a lot of pressure to flood liquid through it or a lot of vacuum to draw material out of the orifice and into the reservoir or the filter between the reservoir and the device.

To prevent the fluid from dripping or running out of the orifice spontaneously, a small positive back pressure (measured in psi, from fractions to a very few) or negative pressure (measured in cm of water, range of a few; in psi, a fraction) can be applied gradually.

9. Repeat the trials described in steps 4-8 until good drop formation is observed.

In many cases, a useful strategy for searching for good pulse shape parameters is to concentrate on the dwell voltage and dwell time. With an echo used, it is common, although not necessary, to keep the echo voltage the negative of the dwell voltage relative to the idle voltage.

Change one parameter at a time in steps of very roughly 10% (e.g., 2 V or 2 µs for standard starting numbers suggested above in step 4). If satellites appear, a reduction of the dwell voltage as well as changes in the dwell and echo times can help to reduce or prevent their occurrence.

10. To stop the pulsing, click on the Stop Jetting button. It will revert to Start Jet Continuous .

- 11. To permanently save a good set of parameters, open the File menu and click on Save Jetting Parameters, which will save the parameters to the last file that has been opened or saved (and always to JETLABDEVICE.DAT), or click on Save As Jetting Parameters to allow yourself to pick an existing or new name for the file.
- 12. If you use the Save As Jetting Parameters entry of the file menu, a standard Windows file save dialog will appear. Provide a file name and click on the Save button. The parameter set can be reloaded later by using the Open Jetting Parameters entry of the File menu. Note that these actions affect the parameters of all jets known at that time in the JetServerTM program.

13. After saving the parameters to a file, the program will automatically return to the main window.

2.2.3 Standard Microdispensing Procedure

- 1. Unpack the syringe.
- 2. Dip the syringe into the liquid and suck it up.
- 3. Put on liquid filter at the top of syringe.
- 4. Put syringe with filter onto liquid reservoir and press liquid slowly through filter into the liquid reservoir.
- 5. Load filtered liquid into dispenser head using a pipette.
- 6. Wipe nozzle tip with lint-free tissue if excess liquid runs out of it.
- 7. Push down dispenser head gently into the holder using two fingers.
- 8. Ensure the power that the laser receives from the power supply is set at 0.1W.
- 9. Set standard settings on JetServer program.
- 10. Set 'Trigger Source' on JetServer program to Internal.
- 11. Set 'Trigger Mode' on JetServer program to Single.
- 12. Hit 'Trigger Jet' on JetServer program.
- 13. Liquid runs out of the nozzle of the dispenser head as a smooth jet.
- 14. To check whether a droplet is visible, 'Strobe delay' can be activated. A stable droplet is visible by Strobe delay = $500\mu s$.

Note:

- Be careful that no particles will contaminate the dispenser head.
- Flush out dispenser head with distilled water after experiment is completed.

2.3 Using an Electrodynamic Balance (EDB) to Study High Total Dissolved Salt Microdroplets

In an electrodynamic balance, a charged particle with a usual radius of 2 to 10 μ m is levitated.⁷ Using automatic mass flow controllers, the lab air/H₂O ratio of steady gas flow is adjusted to modulate the RH. In an experiment, the temperature is dictated by lab conditions while the relative humidity is altered gradually. The sensor is immediately calibrated in the trap using the relative humidity of various salts during deliquescence. Between 10%RH and 80%RH and above 80%RH, its precision is \pm 1.5%RH and \pm 3%RH, respectively.

A Nd:YAG laser (532 nm) illuminates the particle from below in order to visualize it. The DC voltage is adjusted to account for the gravitational force using an automated feedback loop and a video image of the particle captured on a CCD detector.³³ Therefore, a shift in DC voltage can be used as a direct indicator of a mass change. We can determine the mass growth factor if the voltage under dry conditions (RH<10%) correlates to the particle's dry mass (M_{dry}).

2.3.1 EDB Operation

An electrodynamic balance can be used to suspend a micron-sized charged particle in air within a narrow region. A Millikan type DC field acting against gravitation is layered here with a non-uniform alternating field with a concentrating effect. In the null point of the non-uniform field, the charged particle is retained in space. The direct current field is applied between two endcap electrodes, and the alternating field is applied to two electrodes above and below the midplane.

The balance is housed in a three-walled glass chamber with a cooling liquid flowing through the inner walls and a vacuum isolation between the outer walls. The chamber is continually pumped with a constant flow of an appropriate gas mixture, and the total pressure can be changed between 150 and 1000 hPa.33

2.4 Software Used

This section contains experimental data pertaining specific as well as adjusted settings used to run two software programs namely, the JetServer program and EDB software (LabView) with the aim of achieving a goal which is to trap levitated droplets in both chambers (Top Balance and Bottom Balance) of the EDB device. The dispenser should not make droplets that are too small in order to show up on the camera.

Below is a distinct image showing the interface of one of the software programs that I used whilst performing my experiments in the lab.

Figure 8: *JetServer4 Program Interface, MicroFab Technologies, Inc., User's Guide, June 2012, Version 4.1.*

All accessory devices needed for the EDB device to generate droplets must be rightly calibrated, operated and functioning in order for these two software programs to run effectively. For all experiments carried out so far, the main solution used has been sodium chloride (NaCl),

and a saved (default) setting for the JetServer4 application was used for trapping a \sim 20 μ m droplet of 5wt% NaCl.

2.4.1 JetServer4 & EDB Software Settings

Table 1: *Standard JetServer setting used for 5wt% NaCl.*

2.4.2 Target

Merging two droplets for a 5wt% NaCl with 50µm capillary. A single droplet got trapped with no accompanying satellite in both the Top and Bottom Balance which was finally merged successfully as a single droplet with specific settings used.

Note:

• I utilized MicroLev LLC's proprietary LabView software for experimental data collection and control (especially with the voltage).

TOP BALANCE SETTING					
JetServer4			EDB		
Rise Time 1	$3\mu s$	Induction Voltage	$-350V$		
Dwell Time	$25\mu s$	Top Balance	125V		
Fall Time	$9\mu s$	Bottom Balance	0V		
Echo Time	$40\mu s$	Amplitude	500m		
Rise Time 2	$3\mu s$	Frequency	300Hz		
Idle Voltage	0V	Total Flow	60sccm		
Dwell Voltage	14V	Wet Flow	60%		
Echo Voltage	$-20V$	Dry Flow	40%		
Frequency	240Hz				

Table 2: *Top Balance setting used for 5wt% NaCl.*

BOTTOM BALANCE SETTING					
JetServer4			EDB		
Rise Time 1	$3\mu s$	Induction Voltage	150V		
Dwell Time	$25\mu s$	Top Balance	0V		
Fall Time	$3\mu s$	Bottom Balance	$-150V$		
Echo Time	$40\mu s$	Amplitude	500m		
Rise Time 2	$3\mu s$	Frequency	300Hz		
Idle Voltage	0V	Total Flow	60sccm		
Dwell Voltage	18 _V	Wet Flow	60%		
Echo Voltage	$-20V$	Dry Flow	40%		
Frequency	240Hz				

Table 3: *Bottom Balance setting used for 5wt% NaCl.*

Certain observations were made, and comments noted whiles conducting these experiments to get a single droplet merged from two droplets. Amongst them are:

- Feedback button on EDB software program (LabView) automatically adjusts Bottom balance once a droplet is loaded there.
- Reduction of dwell voltage (by 2V) as well as changes of dwell and echo time can help reduce satellite generation.
- Change in frequency value has no impact on droplet size.
- A single trigger mode was used to get trapped droplets.
- If the droplet's image is offset, adjust the Bottom voltage for a centered image.

In the next chapter, I discuss a Theoretical Background as a method for relating the measured voltage to the droplet mass in a sensitive fashion.

3.0 THEORETICAL BACKGROUND

3.1 Force balance: gravity, charge, and drag

The main reason for deriving the force balance is to comprehend the dynamical behavior of levitated multi-drop and single-drop systems. The forces that are acting on the levitated drops must be included in the simulation of the system in order to do this. The principal forces include the gravitational force, the force of mutual Coulombic repulsion, the force of dissipation caused by viscous drag, and the dielectrophoretic force resulting from the interaction of the droplet's internal polarization with the spatial gradient of the electric field.

Here, force balance as used in the water activity paper by Liang et al. 26 will be described mathematically, and details of how it can apply to data gathered during NaCl experiment will be stated.

If there is no relative motion between the particle and the ambient gas, the electrostatic force will be equal to the weight of the particle. The mass of the particle, *m*, can then be determined by:

$$
mg = \frac{c_o q}{z_o} V_{bal} \tag{3.1}
$$

where c_0 , is a balance calibration constant, q is the number of electrostatic charges carried by the particle, V_{bal} is the dc volt- age required to balance the particle, g is the gravitational constant, and z_0 , is the distance between the top and bottom electrodes.

A new equation emerges if a drag force (F_D) is included in the force balance on a particle with air flow:

$$
mg = \frac{c_o q}{z_o} V_{bal, drag} - 6\pi \mu u a \tag{3.2}
$$

where α is the radius of a known particle size for calibration, typically polystyrene latex (PSL) particles, and u is the approach velocity of the particle which is taken to be the velocity at the null

point of the EDB. At 20°C, the viscosity of air stream, p, is 1.82 X Pa.s ²⁷.

$$
F_D = 6\pi \mu u a \text{ [In the EDB, at rest]}
$$
 (3.3)

The equation can be re-written as;

$$
mg = \frac{c_o q}{z_o} V_{bal, drag} - F_D \tag{3.4}
$$

Also,

$$
u = (V_p - V_{air}) \tag{3.5}
$$

where V_p is the velocity of the particles and V_{air} is the velocity of air, so *u* is the relative velocity between particles and air.

In the balance,
$$
V_p = 0
$$
 (3.6)

Hence,

$$
F_D = 6\pi\mu V_{air}a\tag{3.7}
$$

Furthermore,

$$
\dot{m}_{air} = \rho_{air} A V_{air} = \rho_{air} Q \tag{3.8}
$$

where \dot{m}_{air} is the mass flow rate of air, ρ_{air} is the density of air, A is the cross-sectional area of the dispenser tube and Q is the volumetric flow rate.

$$
V_{air} = \frac{\dot{m}_{air}}{\rho_{air}A} = Q \tag{3.9}
$$

$$
Q = AV_{air} \; ; \; V_{air} = \frac{Q}{A} \tag{3.10}
$$

Mass of particle,

$$
m = \rho_p V_p \tag{3.11}
$$

$$
m = \rho_p \left(\frac{4}{3}\pi r_p^3\right) = \rho_p \left(\frac{4}{3}\pi a^3\right) \tag{3.12}
$$

where ρ_p is the density of the particles and r_p is the radius of the particles.

$$
3m = \rho_p 4\pi a^3 \tag{3.13}
$$

$$
a^3 = \frac{3m}{\rho_p 4\pi} \tag{3.14}
$$

$$
a = \left(\frac{3m}{\rho_p 4\pi}\right)^{\frac{1}{3}}\tag{3.15}
$$

Putting $a = \left(\frac{3m}{\rho_p 4\pi}\right)$ & ³ into $mg = \frac{c_o q}{z_o} V_{bal,drag} - 6\pi \mu u a$ gives;

$$
mg = \frac{c_o q}{z_o} V_{bal,drag} - 6\pi \mu u \left(\frac{3m}{\rho_p 4\pi}\right)^{\frac{1}{3}}
$$
(3.16)

$$
m_0 g = m_0 g \frac{V_{bal,drag,0}}{V_{bal,0}} - 6\pi \mu u \left(\frac{3m_0}{\rho_p 4\pi}\right)^{\frac{1}{3}}
$$
(3.17)

$$
mfs_0 = \frac{m_{dry}}{m_0} \tag{3.18}
$$

where $V_{bal,drag,0}$ and $V_{bal,0}$ are the balancing dc voltages of the particles equilibrated at RH₁, with and without the air flow are measured, m_0 is the initial mass of the droplet, mfs_0 is the initial mass fraction of solute and m_{dry} is the dry mass of the particle.

The density, ρ , is a function of mfs and can be obtained from literature data ²⁷ or approximated from an established mixing rule from the literature.²⁸

3.1.1 Droplet mass measurements

$$
mg = \frac{c_o q}{z_o} V_{bal,drag} - 6\pi \mu u \left(\frac{3m}{4\pi \rho_p}\right)^{\frac{1}{3}}
$$
(3.1.1)

Multiplying through the equation by the denominator $[(4\pi \rho_p)^{\frac{1}{3}}z_o]$ gives;

$$
(4\pi \rho_p)^{\frac{1}{3}} z_o mg = (4\pi \rho_p)^{\frac{1}{3}} c_o q V_{bal,drag} -
$$

6 $\pi \mu u (3m)^{\frac{1}{3}} z_o$ (3.1.2)

Grouping like terms gives;

$$
\left(4\pi\rho_p\right)^{\frac{1}{3}}c_o q V_{bal,drag} = \left(4\pi\rho_p\right)^{\frac{1}{3}} z_o mg + 6\pi\mu u (3m)^{\frac{1}{3}} z_o \tag{3.1.3}
$$

Dividing both sides of the equation by $[\left(4\pi\rho_{p}\right)]$ & $\left[{}^{3}\text{C}_{0}q \right]$ reduces the equation to;

$$
V_{bal,drag} = \frac{z_o mg}{c_o q} + \frac{6\pi\mu u (3m)^{\frac{1}{3}} z_o}{(4\pi\rho_p)^{\frac{1}{3}} c_o q}
$$
(3.1.4)

Re-arranging the terms in the equation gives;

$$
V_{bal,drag} = \frac{z_o mg}{c_o q} + \frac{6\pi \mu u z_o}{c_o q} \left(\frac{3m}{4\pi \rho_p}\right)^{\frac{1}{3}}
$$
(3.1.5)

This derivation will be used to interpret the data described in the Results and Discussion section of this document, and all future data. It will also be useful in determining the water activity and hygroscopicity of levitated microdroplets in the electrodynamic device.

4.0 RESULTS AND DISCUSSION

4.1 Initial tests of hygroscopic behavior of NaCl particle

Five different droplets were studied, all containing 5wt% NaCl. Table 4 contains the experimental conditions. The two parameters that I varied were the volume flow rate the droplet is subjected to and the wet/dry ratio. Varying the wet/dry ratio serves the purpose of changing the droplet mass due to loss of water vapor (evaporation) or uptake of water vapor (condensation). Appendix A contains the tables with the raw and smoothed experimental data.

The particle size stayed constant throughout the humidifying process up to $RH = 65.5\%$, at which point a slight reduction in size was noticed due to water adsorption in the solid salts' lattice flaws and structural rearrangement inside the crystal lattice. Note that I am estimating RH from the wet/dry flow ratio. From $RH = 67.7$ to 68.0%, a first deliquescence transition was observed, and its size significantly grew. It grew steadily as RH was raised until $RH = 73.7\%$, where the second transition took place. The particle then kept growing as the RH was raised further.

As the RH is raised from 0 to 67.7%, the morphology does not significantly change. However, the particle boundaries start to round at 73.7% RH. It deliquesces at 76% RH and transforms into a solution droplet with a distinct deliquescence sphere. The deliquescence sphere contracts when the RH is decreased from 76% till the ERH of 44% is obtained. It then recrystallizes at this point. This experiment enables a comparison between a pure NaCl particle's hygroscopic behavior and cycle in the EDB device at a specific flow rate, first with noise signals and then with minimum noise signals as seen in Figure 11.

Droplet #	$\mathbf Q$ (sccm)	Vbal/eff start	Vbal/eff end	Vbal/del start	Vbal/del end	Uptake time (min)	Induction voltage	Vel. of air (m/s)	Calculated Q (sccm)
	150	158	105	110	248	8.05	-150	0.0789	150
	200	264	147	147	282	4.633333333	-150	0.1053	200
	250	278	202	207	387	3.266666667	-150	0.1316	250
$\overline{2}$	150	161	101	111	214	18.18333333	-150	0.0789	150
	200	207	145	140	278	12.55	-150	0.1053	200
	250	265	197	208	380	6.2	-150	0.1316	250
	275	314	219	252	445	5.716666667	-150	0.1447	275
	300	391	284	291	1000	1.933333333	-150	0.1579	300
3	150	168	119	126	497	5.666666667	-150	0.0789	150
$\overline{4}$	200	θ	θ	126	40	2.1	-250	0.1053	200
5	200	$\boldsymbol{0}$	$\boldsymbol{0}$	268	1000	3.8	-100	0.1053	200

Table 4: *Data used to analyze the hygroscopicity cycle of different levitated NaCl droplets in the EDB device at specific flow rates during the conduction of the NaCl deliquescence/efflorescence experiment.*

Figure 9: *Comparing the hygroscopicity cycles of NaCl droplet #1 in the EDB device at a flow rate of 150sccm (1) With noise signals (2) With minimum noise signals.*

5.0 CONCLUSION AND FUTURE WORK

Efflorescence and deliquescence (defined in Appendix C) and their hysteresis occur in NaCl salt (an inorganic compound) when levitated inside the EDB at specific settings. Since RH was only estimated from the ratio of wet/dry flow rates, these experiments should be repeated with an RH probe in the chamber. The study of the phase and morphology of various hydrocarbon petrochemicals in inorganic and organic microdroplets using the EDB is possible due to demonstrating that this unique DBET setup and the force balance development in Chapter 3 enables collection of new data on these critical and multi-component solutions. Hence more experimental data is required for further research that will benefit the energy sector.

To be able to draw more definitive conclusions about the results obtained regarding hygroscopicity when these microdroplets are levitated inside the EDB at specific settings, research and additional experiments on other inorganic compounds (CaCl2, MgCl2, NaBr, (NH4)2SO4,...), as well as organic compounds (Citric acid, Glutaric acid,...) should be carried out. Elimination of coagulated hydrocarbons/petrochemicals in organic and inorganic aqueous solutions with the longterm goal of guiding new technologies is required for treating and recycling produced water effluent sustainably.

REFERENCES

- (1) Stephenson, M. T. Components of Produced Water: A Compilation of Industry Studies. *Journal of Petroleum Technology* **1992**, *44* (05), 548–603. https://doi.org/10.2118/23313- PA.
- (2) Krause, P. R. Spatial and Temporal Variability in Receiving Water Toxicity near an Oil Effluent Discharge Site. *Arch Environ Contam Toxicol* **1995**, *29* (4). https://doi.org/10.1007/BF00208383.
- (3) Clark, C. E.; Veil, J. A. *Produced Water Volumes and Management Practices in the United States.*; Argonne, IL (United States), 2009. https://doi.org/10.2172/1007397.
- (4) Salem, F.; Thiemann, T. Produced Water from Oil and Gas Exploration—Problems, Solutions and Opportunities. *J Water Resour Prot* **2022**, *14* (02), 142–185. https://doi.org/10.4236/jwarp.2022.142009.
- (5) Scanlon, B. R.; Reedy, R. C.; Xu, P.; Engle, M.; Nicot, J. P.; Yoxtheimer, D.; Yang, Q.; Ikonnikova, S. Can We Beneficially Reuse Produced Water from Oil and Gas Extraction in the U.S.? *Science of The Total Environment* **2020**, *717*, 137085. https://doi.org/10.1016/j.scitotenv.2020.137085.
- (6) Cooper, C. M.; McCall, J.; Stokes, S. C.; McKay, C.; Bentley, M. J.; Rosenblum, J. S.; Blewett, T. A.; Huang, Z.; Miara, A.; Talmadge, M.; Evans, A.; Sitterley, K. A.; Kurup, P.; Stokes-Draut, J. R.; Macknick, J.; Borch, T.; Cath, T. Y.; Katz, L. E. Oil and Gas Produced Water Reuse: Opportunities, Treatment Needs, and Challenges. *ACS ES&T Engineering* **2022**, *2* (3), 347–366. https://doi.org/10.1021/acsestengg.1c00248.
- (7) Davis, E. J.; Buehler, M. F.; Ward, T. L. The Double‐ring Electrodynamic Balance for Microparticle Characterization. *Review of Scientific Instruments* **1990**, *61* (4), 1281–1288. https://doi.org/10.1063/1.1141227.
- (8) Rader, D. J.; McMurry, P. H. Application of the Tandem Differential Mobility Analyzer to Studies of Droplet Growth or Evaporation. *J Aerosol Sci* **1986**, *17* (5), 771–787. https://doi.org/10.1016/0021-8502(86)90031-5.
- (9) Bzdek, B. R.; Power, R. M.; Simpson, S. H.; Reid, J. P.; Royall, C. P. Precise, Contactless Measurements of the Surface Tension of Picolitre Aerosol Droplets. *Chem Sci* **2016**, *7* (1), 274–285. https://doi.org/10.1039/C5SC03184B.
- (10) Bahadar Zeb, B.; Khan Alam, K.; Armin Sorooshian, A.; Blaschke, T.; Ahmad, I.; Shahid, I. On the Morphology and Composition of Particulate Matter in an Urban Environment. *Aerosol Air Qual Res* **2018**, *18* (6), 1431–1447. https://doi.org/10.4209/aaqr.2017.09.0340.
- (11) Russell, A. G.; Brunekreef, B. A Focus on Particulate Matter and Health. *Environ Sci Technol* **2009**, *43* (13), 4620–4625. https://doi.org/10.1021/es9005459.
- (12) Noguer, P. J. van der L. X. D. K. M. and C. A. J. *IPCC, 2001: Climate Change 2001: The Scientific Basis.*; THE PRESS SYNDICATE OF THE UNIVERSITY OF CAMBRIDGE, 2001.
- (13) McFiggans, G.; Artaxo, P.; Baltensperger, U.; Coe, H.; Facchini, M. C.; Feingold, G.; Fuzzi, S.; Gysel, M.; Laaksonen, A.; Lohmann, U.; Mentel, T. F.; Murphy, D. M.; O'Dowd, C. D.; Snider, J. R.; Weingartner, E. The Effect of Physical and Chemical Aerosol Properties on Warm Cloud Droplet Activation. *Atmos Chem Phys* **2006**, *6* (9), 2593–2649. https://doi.org/10.5194/acp-6-2593-2006.
- (14) Ansari, A. Prediction of Multicomponent Inorganic Atmospheric Aerosol Behavior. *Atmos Environ* **1999**, *33* (5), 745–757. https://doi.org/10.1016/S1352-2310(98)00221-0.
- (15) Colberg, C. A.; Luo, B. P.; Wernli, H.; Koop, T.; Peter, Th. A Novel Model to Predict the Physical State State of Atmospheric H≪Sub≫2≪/Sub≫SO≪Sub≫4≪/ Sub≫/NH≪Sub≫3≪/Sub≫/H≪Sub& ;Gt;2≪/Sub≫O Aerosol Particles. *Atmos Chem Phys* 2003, 3 (4), 909–924. https://doi.org/10.5194/acp-3-909-2003.
- (16) Putaud, J. P.; Raes, F.; Van Dingenen, R.; Brüggemann, E.; Facchini, M. C.; Decesari, S.; Fuzzi, S.; Gehrig, R.; Hüglin, C.; Laj, P.; Lorbeer, G.; Maenhaut, W.; Mihalopoulos, N.; Müller, K.; Querol, X.; Rodriguez, S.; Schneider, J.; Spindler, G.; Ten Brink, H.; Tørseth,

K.; Wiedensohler, A. A European Aerosol Phenomenology—2: Chemical Characteristics of Particulate Matter at Kerbside, Urban, Rural and Background Sites in Europe. *Atmos Environ* **2004**, *38* (16), 2579–2595. https://doi.org/10.1016/J.ATMOSENV.2004.01.041.

- (17) Dick, W. D.; Saxena, P.; McMurry, P. H. Estimation of Water Uptake by Organic Compounds in Submicron Aerosols Measured during the Southeastern Aerosol and Visibility Study. *Journal of Geophysical Research: Atmospheres* **2000**, *105* (D1), 1471– 1479. https://doi.org/10.1029/1999JD901001.
- (18) Marcolli, C.; Luo, B.; Peter, T. Mixing of the Organic Aerosol Fractions: Liquids as the Thermodynamically Stable Phases. *J Phys Chem A* **2004**, *108* (12), 2216–2224. https://doi.org/10.1021/jp036080l.
- (19) Fan, W.; Chen, T.; Zhu, Z.; Zhang, H.; Qiu, Y.; Yin, D. A Review of Secondary Organic Aerosols Formation Focusing on Organosulfates and Organic Nitrates. *J Hazard Mater* **2022**, *430*, 128406. https://doi.org/10.1016/j.jhazmat.2022.128406.
- (20) De Gouw, J.; Jimenez, J. L. Organic Aerosols in the Earth's Atmosphere. *Environ Sci Technol* **2009**, *43* (20), 7614–7618. https://doi.org/10.1021/es9006004.
- (21) Andreae, M. O.; Browell, E. V.; Garstang, M.; Gregory, G. L.; Harriss, R. C.; Hill, G. F.; Jacob, D. J.; Pereira, M. C.; Sachse, G. W.; Setzer, A. W.; Dias, P. L. S.; Talbot, R. W.; Torres, A. L.; Wofsy, S. C. Biomass-Burning Emissions and Associated Haze Layers over Amazonia. *J Geophys Res* **1988**, *93* (D2), 1509. https://doi.org/10.1029/JD093iD02p01509.
- (22) Immler, F.; Engelbart, D.; Schrems, O. Fluorescence from Atmospheric Aerosol Detected by a Lidar Indicates Biogenic Particles in the Lowermost Stratosphere. *Atmos Chem Phys* **2005**, *5* (2), 345–355. https://doi.org/10.5194/acp-5-345-2005.
- (23) Saxena, P.; Hildemann, L. M.; McMurry, P. H.; Seinfeld, J. H. Organics Alter Hygroscopic Behavior of Atmospheric Particles. *J Geophys Res* **1995**, *100* (D9), 18755. https://doi.org/10.1029/95JD01835.
- (24) Choi, M. Y.; Chan, C. K. The Effects of Organic Species on the Hygroscopic Behaviors of Inorganic Aerosols. *Environ Sci Technol* **2002**, *36* (11), 2422–2428. https://doi.org/10.1021/es0113293.
- (25) Rivera-Carpio, C. A.; Corrigan, C. E.; Novakov, T.; Penner, J. E.; Rogers, C. F.; Chow, J. C. Derivation of Contributions of Sulfate and Carbonaceous Aerosols to Cloud Condensation Nuclei from Mass Size Distributions. *Journal of Geophysical Research: Atmospheres* **1996**, *101* (D14), 19483–19493. https://doi.org/10.1029/95JD01077.
- (26) Liang, Z.; Chan, C. K. A Fast Technique for Measuring Water Activity of Atmospheric Aerosols. *Aerosol Science and Technology* **1997**, *26* (3), 255–268. https://doi.org/10.1080/02786829708965427.
- (27) Perry, M. Eddy Current Damping Due to a Linear Periodic Array of Magnetic Poles. *IEEE Trans Magn* **1984**, *20* (1), 149–155. https://doi.org/10.1109/TMAG.1984.1063005.
- (28) Riemer, N.; Ault, A. P.; West, M.; Craig, R. L.; Curtis, J. H. Aerosol Mixing State: Measurements, Modeling, and Impacts. *Reviews of Geophysics* **2019**, *57* (2), 187–249. https://doi.org/10.1029/2018RG000615.
- (29) Richards, D. S.; Trobaugh, K. L.; Hajek-Herrera, J.; Davis, R. D. Dual-Balance Electrodynamic Trap as a Microanalytical Tool for Identifying Gel Transitions and Viscous Properties of Levitated Aerosol Particles. *Anal Chem* **2020**, *92* (4), 3086–3094. https://doi.org/10.1021/acs.analchem.9b04487.
- (30) Richards, D. S.; Trobaugh, K. L.; Hajek-Herrera, J.; Price, C. L.; Sheldon, C. S.; Davies, J. F.; Davis, R. D. Ion-Molecule Interactions Enable Unexpected Phase Transitions in Organic-Inorganic Aerosol. *Sci Adv* **2020**, *6* (47). https://doi.org/10.1126/sciadv.abb5643.
- (31) Miles, R. E. H.; Glerum, M. W. J.; Boyer, H. C.; Walker, J. S.; Dutcher, C. S.; Bzdek, B. R. Surface Tensions of Picoliter Droplets with Sub-Millisecond Surface Age. *J Phys Chem A* **2019**, *123* (13), 3021–3029. https://doi.org/10.1021/acs.jpca.9b00903.
- (32) Davies, J. F. Mass, Charge, and Radius of Droplets in a Linear Quadrupole Electrodynamic Balance. *Aerosol Science and Technology* **2019**, *53* (3), 309–320. https://doi.org/10.1080/02786826.2018.1559921.
- (33) Steimer, S. S.; Krieger, U. K.; Te, Y.-F.; Lienhard, D. M.; Huisman, A. J.; Luo, B. P.; Ammann, M.; Peter, T. Electrodynamic Balance Measurements of Thermodynamic, Kinetic, and Optical Aerosol Properties Inaccessible to Bulk Methods. *Atmos Meas Tech* **2015**, *8* (6), 2397–2408. https://doi.org/10.5194/amt-8-2397-2015.
- (34) Ge, Z.; Wexler, A. S.; Johnston, M. V. *Multicomponent Aerosol Crystallization (NH 4) 2 SO 4 /NH 4 NO 3 Mixed Droplets and Their Results Were*; 1996; Vol. 183.

APPENDIX A

Data Analysis: Hygroscopicity cycles of 5wt% NaCl droplet

2.099	237.9	237.8987592	237.8975267
2.149	237.9	237.8987594	237.8975274
2.199	237.9	237.8987595	237.8975281
2.25	237.9	237.8987597	237.8975289
2.3	237.9	237.8987599	237.8975296
2.35	237.9	237.8987601	237.8975304
\cdots	\cdots	.	\cdots
476.6	141.3	238.063596	221.4099255
476.65	145.3	238.0496815	221.3870925
476.7	146.1	238.035889	221.3645064
476.749	147	238.0222336	221.342197
476.799	147.8	238.0087003	221.3201344
476.849	148.6	237.995289	221.2983183
476.899	145.2	237.9813697	221.2754888
476.949	141.8	237.9669425	221.2516462
477	138.5	237.9520225	221.2268207
477.049	133.4	237.9363397	221.2004726
477.099	128.3	237.9198942	221.1726025
477.149	123.2	237.9026862	221.1432107
477.199	117.8	237.8846708	221.1122078
477.249	112.5	237.8658631	221.0796241
477.299	107.2	237.8462632	221.0454602
477.35	102.1	237.8259013	221.0097766
477.4	97	237.8047774	220.9725736
477.449	91.9	237.7828917	220.9338519
477.499	88.5	237.7604993	220.8941217
477.549	85.1	237.7376002	220.8533835
477.599	81.6	237.7141796	220.8116075
477.649	78.2	237.6902524	220.768824
477.699	77.6	237.6662389	220.7258733
477.75	77	237.642139	220.6827556
477.799	76.4	237.6179526	220.6394707
477.849	79	237.5941599	220.5969789
477.899	81.5	237.5707458	220.5552498
477.949	84	237.5477102	220.5142832
477.999	89.8	237.525548	220.4750689
478.049	95.5	237.5042442	220.4375764
478.1	101.3	237.4838136	220.4018351
478.15	108.6	237.464481	220.3682946
478.199	115.8	237.4462313	220.3369241
478.249	123	237.4290644	220.307723
478.299	129.6	237.41289	220.2805107
478.349	136.2	237.3977081	220.2552866
478.399	142.9	237.3835335	220.23208
478.449	149.5	237.3703509	220.2108603
478.5	152.4	237.3576054	220.1905171
478.549	155.3	237.3452967	220.1710499

Table 5: *Data used to analyze the hygroscopicity cycle NaCl droplet #1 in the EDB device at 150sccm flow rate during the conduction of the NaCl deliquescence/efflorescence experiment (1) With noise signals (2) With minimum noise signals, before efflorescence occurs.*

483.399	120.1	235.553642	129.3928513
483.449	124	235.536909	129.3389228
483.499	127.8	235.5207484	129.3235336
483.549	131.6	235.5051603	129.3462983
483.599	130	235.4893345	129.3528353
483.649	128.3	235.4732561	129.3423069
483.699	126.7	235.4569402	129.3158839
483.75	126.5	235.4405966	129.287725
483.799	126.2	235.4242105	129.2568478
483.849	125.9	235.4077819	129.2232793
483.899	121.8	235.3907407	129.1490465
483.949	117.7	235.3730871	129.034556
483.999	113.6	235.3548212	128.8802105
484.049	109.5	235.3359429	128.6864084
484.1	106.4	235.3166025	128.4635443
484.15	103.2	235.296785	128.2109088
484.199	100.1	235.2765055	127.9297998
484.249	98.9	235.2560491	127.6395018
484.299	97.6	235.2354006	127.3391067
484.349	96.4	235.2145753	127.0297157
484.399	94.7	235.1934982	126.7064185
484.45	93	235.1721691	126.3693543
484.5	91.3	235.1505883	126.0186608
484.549	93.2	235.1292957	125.6904742
484.599	95.2	235.1083063	125.3855694
484.649	97.1	235.0876051	125.1027137
484.699	99.3	235.0672369	124.8446866
484.749 484.799	101.4	235.0471868 235.0274698	124.6102397 124.4001373
484.85	103.6 105.7		124.213136
484.899	109.4	235.0080706 234.9892294	124.0650046
484.949	113	234.9709311	123.9543546
484.999	116.7	234.9531904	123.881811
485.049	118.2	234.9356774	123.8249929
485.099	119.8	234.9184071	123.784743
485.149	121.3	234.9013643	123.7598955
485.199	121	234.8842791	123.7322966
485.25	120.7	234.8671515	123.7019736
485.299	120.3	234.8499664	123.6679539
485.349	120.6	234.8328289	123.6372744
485.399	120.8	234.815724	123.6089016
485.449	121.1	234.7986666	123.5838126
485.499	118.5	234.7812218	123.5329745
485.549	115.9	234.7633896	123.4566447
485.6	113.3	234.7451701	123.3550783
485.649	110.7	234.7265634	123.2285275
485.699	108.8	234.7076744	123.0842422
485.749	106.9	234.6885032	122.9223998
485.799	105.1	234.6690649	

Table 6:*Data used to analyze the hygroscopicity cycle of NaCl droplet #1 in the EDB device at 150sccm flow rate during the conduction of the NaCl deliquescence/efflorescence experiment (1) With noise signals (2) With minimum noise signals, during which efflorescence occurs.*

488.099	114.3	233.8029691		103.9661788
488.149	113.9	233.7849836		103.9691589
488.2	113.5	233.7669409		103.9720182
488.25	112.7	233.7487808		103.9746366
488.299	112	233.7305185		103.9770442
\cdots	.	.		
1395.049	200	312.0805042		412.9265489
1395.1	200	312.0636921		412.862671
1395.15	200	312.0468826		412.7988122
1395.2	200	312.0300756		412.7349725
1395.249	200	312.013271		412.671152
1395.299	200	311.9964691		412.6073507
1395.349	200	311.9796696		412.5435685
1395.399	200	311.9628726		412.4798054
1395.45	200	311.9460782		412.4160615
1395.5	200	311.9292863		412.3523367
1395.55	200	311.9124969		412.288631
1395.599	200	311.89571		412.2249444
1395.649	200	311.8789257		412.1612769
1395.699	200	311.8621438		412.0976285
1395.749	200	311.8453645		412.0339992
1395.799	200	311.8285877		411.970389
1395.85	200	311.8118134		411.9067979
1395.9	200	311.7950416		411.8432259
1395.95	200	311.7782724		411.7796729
1395.999	200	311.7615056		411.716139
1396.049	200	311.7447414		411.6526241
1396.099	200	311.7279797		411.5891284
1396.149	200	311.7112205		411.5256516
1396.2	200	311.6944638		411.4621939
1396.25	200	311.6777097		411.3987553
1396.3	200	311.660958		411.3353356
1396.349	200	311.6442089		411.271935
1396.399	200	311.6274622		411.2085535
1396.449	200	311.6107181		411.1451909
1396.499	200	311.5939765		411.0818473
1396.55	200	311.5772374		411.0185228
1396.6	200	311.5605008		410.9552172
1396.65	200	311.5437667		410.8919307
1396.7	200	311.5270352		410.8286631
1396.749	200	311.5103061		410.7654145
1396.799	200	311.4935796		410.7021849
1396.849	200	311.4768555		410.6389742
1396.899	200	311.460134		410.5757825
1396.95	200	311.443415		410.5126098
1397	200	311.4266985		410.449456
1397.05	200	311.4099845		410.3863212
1397.099	200			

Table 7: *Data used to analyze the hygroscopicity cycle of NaCl droplet #1 in the EDB device at 150sccm flow rate during the conduction of the NaCl deliquescence/efflorescence experiment (1) With noise signals (2) With minimum noise signals, after efflorescence occurs.*

APPENDIX B

Data Smoothing: Comparison of hygroscopicity cycles of 5wt% NaCl droplet before, during and after efflorescence

Figure 10: *Comparing the hygroscopicity cycles of NaCl droplet #1 in the EDB device at a flow rate of 150sccm (1) With noise signals (2) With minimum noise signals, before efflorescence occurs.*

Figure 11: *Comparing the hygroscopicity cycles of NaCl droplet #1 in the EDB device at a flow rate of 150sccm (1) With noise signals (2) With minimum noise signals, during efflorescence occurs.*

Figure 12: *Comparing the hygroscopicity cycles of NaCl droplet #1 in the EDB device at a flow rate of 150sccm (1) With noise signals (2) With minimum noise signals, after efflorescence occurs.*

Figure 13: *Hygroscopicity cycle of 3 different NaCl droplets in the EDB device at a flow rate of 150sccm.*

Figure 14: *Hygroscopicity cycle of 4 different NaCl droplets in the EDB device at a flow rate of 200sccm.*

Figure 15: *Hygroscopicity cycle of 2 different NaCl droplets in the EDB device at a flow rate of 250sccm.*

Figure 16: *Hygroscopicity cycle of a NaCl droplet in the EDB device at a flow rate of 275sccm.*

Figure 17: *Hygroscopicity cycle of a NaCl droplet in the EDB device at a flow rate of 300sccm.*

APPENDIX C

Definitions

Chemical Potential

The chemical potential of a specie in thermodynamics is the energy that can be absorbed or released owing to a change in the particle number of the given species, such as in a chemical reaction or phase transition. The chemical potential of a species in a mixture is defined as the rate of change of a thermodynamic system's free energy with regard to the number of atoms or molecules of the species introduced to the system. As a result, it is the partial derivative of the free energy with respect to the amount of the species, with the concentrations of all other species in the mixture remaining constant.

The chemical potential is the **partial molar Gibbs free energy** when both temperature and pressure are held constant, and the number of particles is represented in moles. The whole sum of the product of chemical potentials and stoichiometric coefficients is zero in chemical equilibrium or in phase equilibrium because the free energy is at a minimum. The chemical potential of any chemical species is universally the same throughout a system in diffusion equilibrium.

The chemical potential drives mass transfer in the same way that the thermal potential drives heat transfer from higher to lower temperatures.

Chemical Equilibrium

Chemical equilibrium is the thermodynamic equilibrium in a system that allows for both direct and reverse chemical reactions. If the system achieves chemical equilibrium, the rates of all reactions proceeding in opposite directions are equal. As a result, the system's macroscopic parameters remain constant, and the relationship between the concentrations of reactive components remains constant at any given temperature. In a chemical reaction equation,

equilibrium is expressed by the equality $\sum \nu_i \mu_i = 0$, where μ_i is the chemical potential of each reagent $(i = 1, 2, ...)$ and vi is the stoichiometric coefficient of each substance (it is positive for initial substances and negative for products of a reaction).

Chemical equilibrium exists when a system's chemical composition does not change. For example, if an arbitrary combination of H_2 , O_2 , and H_2O is enclosed in a vessel at a specified temperature and pressure and no future change in chemical composition occurs, the system is in chemical equilibrium. It should be noted that the three species are permitted to react chemically, with the restriction that the number of moles of a species consumed must match the number of moles produced, i.e., there is no net change in the concentration of any species.

Mole Fraction

The mole fraction or **molar fraction** $(x_i \text{ or } x_i)$ in chemistry is defined as a unit of a constituent's amount (expressed in moles), *ni*, divided by the total amount of all constituents in a mixture (also represented in moles), n_{tot} . This expression is as follows:

$$
x_i = \frac{n_i}{n_{tot}}
$$

The sum of all the mole fractions is equals 1:

$$
\sum_{i=1}^{N} n_i = n_{tot}; \sum_{i=1}^{N} x_i = 1.
$$

The mole percent, molar percentage, or molar proportion (mol%) is the same notion represented with a denominator of 100. Amount fraction is another name for the mole fraction. It is the same as the number fraction, which is defined as the number of molecules of a constituent Ni divided by the total number of molecules Ntot. The mole fraction is a dimensionless quantity that can be used to indicate the composition of a mixture.

Raoult's Law

The vapor pressure of a solvent above a solution, according to Raoult's law, is equal to the vapor pressure of the pure solvent at the same temperature scaled by the mole fraction of the solvent present:

 $P_{solution} = \chi_{solvent} P^{o}_{solvent}$

Non-Ideal Solution

A non-ideal solution is one that deviates from the ideal solution's norms, in which the interactions between molecules are the same (or extremely similar) to those between molecules of different components. That is, no Van der Waals nor Coulomb forces, nor any other kind of force, are acting between the parts. We presume that diluted solutions have ideal properties.

Thermodynamic Activity

Activity (symbol a) is a measure of a species' "effective concentration" in a mixture according to chemical thermodynamics. This means that the chemical potential of a species depends on the activity of a real solution just as it would depend on concentration for an ideal solution.

Activity is typically thought of as a dimensionless quantity, despite the fact that its value relies on the species' chosen standards of normal behavior. Pure substance activity in condensed phases (solid or liquid) is typically regarded as unity (the number 1). In addition to other factors, activity is influenced by the mixture's composition, pressure, and temperature. The effective partial pressure, also known as fugacity, is the activity for gases.

Because interactions between different types of molecules in non-ideal gases or liquids differ from interactions between the same types of molecules, there is a discrepancy between activity and other measurements of concentration. The environment has a significant impact on an ion's activity.

Molality

The number of moles of solute in a solution equal to 1 kg or 1000 g of solvent is referred to as its molality. The definition of molarity, on the other hand, is based on a certain volume of solution.

'mol/kg' is a typical molality measurement unit in chemistry. One molal is another way to refer to a solution with a concentration of 1 mol/kg. Molar mass must be represented in *kg/mol* rather than the more common *g/mol* or *kg/kmol* when using the unit *mol/kg*.

The amount of substance (in moles) of the solute, n_{solute} , divided by the mass (in kg) of the solvent, $m_{solvent}$, determines a solution's molality (b):

$$
b = \frac{n_{solute}}{m_{solvent}}
$$

When there are multiple solvents present in a solution, the molality of the mixed solvent can be determined by treating it like a pure pseudo-solvent. Units are defined as mole solute per kilogram mixed solvent rather than mole solute per kilogram solvent as in the binary case.

Electrolyte Solutions

A solution known as an electrolyte is one that is electrically conductive and typically contains ions, which are atoms or molecules that have received or lost electrons. They are frequently referred to as ionic solutions because of this, however there are some situations in which the electrolytes are not ions.

The idea that like charges repel and opposite charges attract is a fundamental tenet of

electrostatics. The electrostatic attraction is likewise very difficult to overcome.

Aerosol Liquid Water Content (ALWC)

To determine the mass of water absorbed by a unit volume of dry aerosol, the relative ALWC is defined as the ratio between ALWC and the dry aerosol volume V_{dry} .

The relative ALWC can be used as a stand-in for an aerosol species' hygroscopicity.

Chemical Potential of water

Water's chemical potential is defined as the free energy per mole of water. Simply described, chemical potential is the ability of a substance to react or move, or to conduct work. When a force is applied to an object, it moves from one position to another.

Water potential is the chemical potential of water, and its value is proportional to the quantity of water molecules in the system. The combination of solute potential plus pressure potential yields water potential. The potential for solute is negative, but the potential for pressure is positive.

Temperature Dependence of Relative Humidity (RH)

With the same absolute/specific humidity, air in a cooler environment will have a higher relative humidity than air in a warmer environment because warmer air may contain more water vapor (moisture).

The quantity of water vapor that the air is currently carrying as compared to what it would be holding if it were saturated is known as relative humidity. For instance, if the relative humidity is 20%, the air has 20% of the water vapor it is capable of holding at that temperature. However, as the air's ability to contain water vapor increases with temperature, the relative humidity drops.

Solubility of Aerosol Salts as a Function of Temperature

Effect of temperature on liquid and solid solutes

Depending on whether the dissolution reaction is exothermic or endothermic, a solid or liquid's solubility may change as temperature rises.

Solubility increases as temperature rises

- In endothermic dissolution reactions, heat energy is absorbed into the system as the solute dissolves due to the net energy from breaking and creating bonds. Additional head energy is added to the system when the system's temperature rises.
- Le Chatelier's Principle states that the system will respond to this rise in temperature by encouraging the dissolving reaction to absorb the extra heat energy. Solubility of the solute will consequently increase as temperature rises.
- Ammonium nitrate, which is used in first-aid cold packs, is an example of a solute whose solubility rises with increasing temperature. An endothermic process occurs when ammonium nitrate dissolves in solution. As the ammonium nitrate dissolves, heat energy from the surroundings is absorbed, making the area feel cold.

Decreasing solubility as temperature rises

- When a solute dissolves in a solution, heat energy is released in an exothermic reaction. More heat enters the system as the temperature rises. The system will respond to this extra heat energy by limiting the dissolving reaction, in accordance with Le Chatelier's Principle. The solute is therefore less soluble at higher temperatures.
- Calcium hydroxide, which is used as an antacid and to treat chemical burns, is an example of a solute whose solubility declines with temperature.

Deliquescence

A substance collects moisture from the air through the process of deliquescence, which continues until the substance dissolves in the water and produces a solution. Deliquescence happens when the solution's produced vapor pressure is lower than the partial pressure of airborne water vapor.

If the air is sufficiently humid, all soluble salts will dissolve. A substance is referred to as hygroscopic if it can absorb moisture from the air without necessarily dissolving.

Efflorescence

When exposed to air at room temperature, crystalline molecules exhibit efflorescence, which is the loss of water. A chemical substance absorbs moisture from the air and dissolves in it to form a solution through the process of deliquescence.

Efflorescence happens when the hydrate's aqueous vapor pressure is higher than the partial pressure of the air's water vapor.

Multicomponent Aerosols

Only at the eutonic point do particles dried from multicomponent aqueous aerosols have a homogeneous chemical shape, according to thermodynamic study. The particles are made up of a pure salt core surrounded by a mixed salt coating, where the coating's chemical makeup is similar to the eutonic point and is unaffected by the original component mole fractions while the core's composition is exclusively dictated by the original aerosol's composition. 34