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# Research on multi-timescale operation optimization of a distributed electro-hydrogen coupling system considering grid interaction

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Against the backdrop of increasingly prominent environmental issues, new energy consumption issues, and energy supply and demand balance issues, the optimization of multi time scale operation of distributed electro hydrogen coupling systems has become a research focus. Based on this, this article optimizes the multi time scale operation of a distributed electric hydrogen coupling system that takes into account grid interaction. By designing a system framework for distributed electro hydrogen coupling systems, operational strategies for each system were proposed. Analyzed the uncertainty and response characteristics of wind and solar power generation units and load demand, and constructed a multiple uncertainty model for distributed electric hydrogen coupling system. At the same time, a three stage, multi time scale operation optimization model of the electric hydrogen coupling system was constructed based on the response characteristics of the distributed electric hydrogen coupling system. The construction of these models reduced scheduling costs by 12.55% and increased clean energy consumption rate by 13.50%.

## KEYWORDS

multiple uncertainties, electro-hydrogen coupling, multi-timescale, operational optimization, grid interaction

## 1 Introduction

Under the “dual carbon” goal, environmental issues and energy supply and demand balance are becoming increasingly prominent (Ren et al., 2022). In this context, the production of clean wind and solar new energy has developed on a large scale, but problems such as uncertainty, volatility, and inability to fully absorb remain unresolved (Li et al., 2022). Utilizing uncontrollable wind and solar new energy to generate hydrogen and locally supply regional hydrogen load demand can reduce transportation costs. At the same time, hydrogen energy, as a secondary energy source, has advantages such as flexible conversion and long-term energy storage (Gorre et al., 2020; Zhang et al., 2022). Therefore, coupling the electric energy network with the hydrogen energy network into an electric hydrogen system has significant economic value (Zhang et al., 2022). Optimizing the operation of the coupling system lays the foundation for the development of distributed electric hydrogen coupling systems. However, at different timescales, the accuracy of wind,

photovoltaic, and load prediction in the electric hydrogen coupling system is inconsistent (Li et al., 2022). It is necessary to conduct research on the multi-timescale operation of the electric hydrogen system.

Regarding research on multiple timescales, most of the existing research focuses on integrated energy systems. Based on the differences in energy characteristics in integrated energy systems, Li et al. (2020) optimized the scheduling time resolution of cooling, heating, and electricity and constructed a mixed day-to-day timescale scheduling optimization model for integrated energy systems. Xu et al. (2019) designed a comprehensive response architecture that considers multiple timescales to achieve orderly scheduling of user demand responses, which can reduce overall operating costs. Wang et al. (2022) proposed a two-stage scheduling optimization plan with the objective function of minimizing operating costs, taking the combined cooling, heating, and power system as the research object. Jin et al. (2019) focused on microgrid systems and also proposed a two-stage scheduling optimization plan. On the basis of the two-stage rolling optimization of “day-ahead-day-in,” Yuan et al. (2019) (Bao et al., 2016) proposed a multi-timescale scheduling optimization method that considers “day-ahead-day-in-real-time,” where day-ahead takes 1 h as the scheduling response time, the day-in response time is 15 min, and the real-time response time is 5 min. Furthermore, based on the optimization of “day-ahead-day-in-real-time,” Zhao et al. (2020) proposed a long-term optimization model with an annual cycle, with the objective function of minimizing annual investment cost, to optimize the capacity allocation and investment decision-making of the comprehensive energy system. From the existing multi-timescale optimization research, on the one hand, there is a lack of operational optimization research focusing on distributed electro-hydrogen coupling systems in the research object. On the other hand, in terms of multi-timescale research, the growth of scheduling response time is mostly 1 h in the day-ahead, 15 min in the day-in, and 5 min in the real-time, without in-depth consideration of equipment and energy characteristics.

In the operation process of distributed electric hydrogen coupling systems, due to the existence of multiple uncertainties in wind power, photovoltaic, and load, the study of uncertainty is also crucial for distributed electric hydrogen coupling systems. Pan et al. (2022) used robust coefficients to characterize the uncertainty of renewable energy sources and other sources. Hou et al. (2021) described the uncertainty of wind and solar output based on the typical scenario method. Lu et al. (2022) used the interval method to describe the uncertainty of user-end load. In addition to considering the unilateral uncertainty of the source and load ends, Cui et al. (2022) (Zhai et al., 2020) also considered the uncertainty of new energy generation and comprehensive demand response and verified through examples that considering multiple uncertainties can improve the risk resistance ability of the comprehensive energy system. The existing research on uncertainty can consider the uncertainty of source-side output and load-side demand response. However, in distributed electro-hydrogen coupling systems, demand response is an important

resource for its invocation, and the accuracy of resource invocation will also affect the uncertainty of the system. Existing research has little consideration for the uncertainty of load-side demand response.

Based on the aforementioned research, this paper conducts a multi-timescale operation optimization study of a distributed electric hydrogen coupling system that takes into account grid interaction. Compared with the existing research, this work incorporated the following innovations:

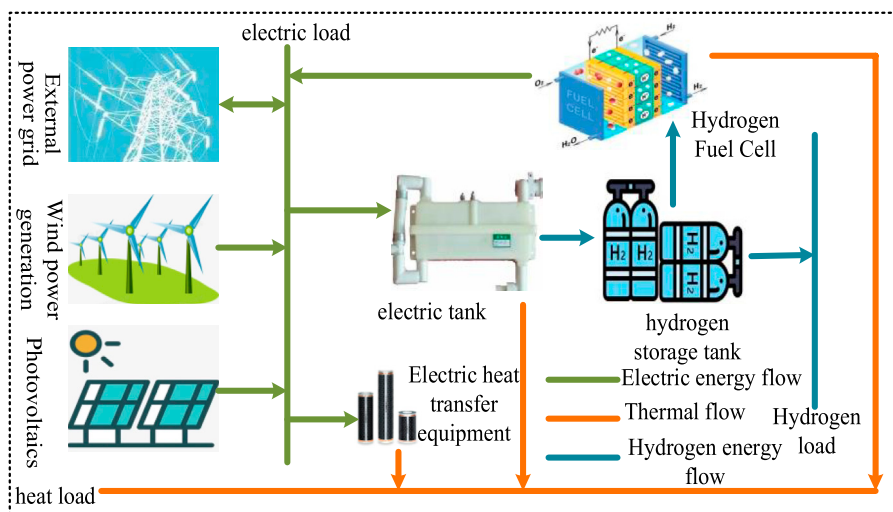
- (1) In terms of uncertainty analysis, not only the uncertainty of the source and load ends is considered, but also the uncertainty of the load demand response in the coupled system is innovatively considered.
- (2) In terms of operational optimization, based on the response characteristics of the equipment, a three-stage multi-timescale operational optimization model of “day-ahead-day-in-real-time” is proposed. Considering the adjustment and response level of equipment in the day-in and real-time stages, a “day-in-real-time” two-stage adjustment plan is developed, which differs from traditional overall adjustment.
- (3) In terms of scheduling time, the traditional response scheduling time of 1 h in the day-ahead, 15 min in the day-in, and 5 min in the real-time is optimized based on system equipment and various energy characteristics.

The remainder of this paper is arranged as follows: in Section 2, the framework of the electric hydrogen coupling system is designed, and the operation strategy of the coupling system unit is proposed. In Section 3, based on the system unit modeling, the uncertainty and response characteristics of the coupled system are analyzed. In Section 4, a coupled system operation optimization model with three timescales of day before day, day within day, and real time is constructed. In Section 5, taking a coupled system as an example for empirical analysis, the effectiveness of the model was verified.

## 2 Design of the electric hydrogen coupling system

### 2.1 System framework

The electric hydrogen coupling system includes three networks: electric energy network, hydrogen network, and thermal network. The distributed power supply network consists of wind turbines, photovoltaic panels, external networks, and electrical loads. The hydrogen network consists of an electrolytic cell, hydrogen fuel cell, hydrogen storage tank, and hydrogen load. The thermal energy network is composed of electric to heat equipment, electrolytic cell, and cooling water circulating device inside the hydrogen fuel cell. Distributed power supply, hydrogen network, and thermal network are coupled together and coordinated and dispatched by the control center of the electric hydrogen coupling system. When there is a shortage demand in the coupling system, energy is purchased from external networks. If the system exceeds supply, energy is sold to external networks (Figure 1).



**FIGURE 1**  
Framework diagram of the electric hydrogen coupling system.

## 2.2 System unit operation strategy

### 2.2.1 Electric energy network

In order to reduce wind and solar power abandonment rates and achieve the consumption of wind and photovoltaic power generation, the control center of the electric hydrogen coupling system conducts full scheduling of wind and photovoltaic power generation. On the one hand, when wind power and photovoltaic power cannot meet the electricity load demand, electricity is purchased from the external grid to meet the electricity load demand shortage. On the other hand, the hydrogen is released from the hydrogen storage tank and generated by the hydrogen fuel cell. When wind and photovoltaic power generation exceeds the electricity load demand, the electrolysis cells use the excess electricity to produce hydrogen, and the generated hydrogen is stored in hydrogen storage tanks to supply the local hydrogen load demand.

### 2.2.2 Hydrogen energy network

When wind and photovoltaic power generation exceeds the electricity load demand, the electrolytic cell uses excess electricity to produce hydrogen, and combined with the electricity price situation, the generated hydrogen is stored in the hydrogen storage tank. If the power load of the system is insufficient and the electricity price is high, the hydrogen in the storage tank will be supplied to the hydrogen fuel cell to generate electric energy and heat energy to obtain benefits. If the system's electricity load is insufficient, the electricity price is low, and the purchased electricity meets the system's electricity load demand with higher efficiency, the generated hydrogen will be stored in hydrogen storage tanks to supply the regional hydrogen load demand.

### 2.2.3 Thermal network

The heat load demand of the thermal energy network is met by the electric-to-heat equipment, hydrogen fuel cell, and electrolytic cell. Among them, the heating efficiency of hydrogen fuel cells is higher than the power supply efficiency. In hydrogen fuel cells, we first consider the heat load demand to control the hydrogen consumption of hydrogen

fuel cells and then consider the power load demand. Therefore, hydrogen fuel cells and electrolytic cells are first used to meet the heat load demand in the heat energy network. If hydrogen fuel cells and electrolytic cells cannot meet the heat load demand, then the power is purchased from the external network or the excess power from wind and solar power generation is used to supply heat through the electric-to-heat equipment.

## 3 Unit modeling and uncertainty analysis of the electro-hydrogen coupling system

### 3.1 System unit modeling

This section considers the characteristics of each unit equipment and constructs corresponding models.

#### 3.1.1 Wind turbines

The output of wind power at each moment is the product of the installed capacity and output coefficient of the wind power plant, as shown in Eq. 1:

$$P_{wind,t} = \eta_{wind,t} \cdot P_{wind}^e \tag{1}$$

where  $P_{wind,t}$  is the output of the wind power plant at time  $t$ ;  $\eta_{wind,t}$  is the output coefficient of the wind power plant at time  $t$ ; and  $P_{wind}^e$  is the rated power of the wind power plant.

#### 3.1.2 Photovoltaic unit

Photovoltaic power generation is influenced by regional light intensity, and the beta distribution is used to fit the radiation pattern of light. The output of photovoltaic power generation is shown in Eq. 2:

$$P_{pv,t} = m_{pv} \cdot f_{pv,t} \cdot \lambda_{pv} \cdot \lambda_{tran} \cdot (1 - \lambda_{loss}), \tag{2}$$

where  $P_{pv,t}$  is the photovoltaic power generation output at time  $t$ ;  $m_{pv}$  is the area of the photovoltaic panel;  $f_{pv,t}$  is the light intensity

at time  $t$ ;  $\lambda_{pv}$  is the efficiency of the photovoltaic panel in absorbing light intensity;  $\lambda_{tran}$  is the solar-cell efficiency; and  $\lambda_{loss}$  is the loss coefficient of the photovoltaic panel.

### 3.1.3 Electric tank

Electrolytic cells include an alkaline electrolyzer, a high-temperature steam electrolyzer, and a proton-exchange membrane electrolyzer. Due to their advantages of easy maintenance and wide application (Liu et al., 2022), alkaline electrolyzers are suitable for the electric hydrogen coupling system constructed in this paper for park scenarios. Based on this, an alkaline electrolytic cell is used in this section. The real-time balance between the electrical energy consumed and the energy generated during the operation of an alkaline electrolytic cell is shown in Eq. 3:

$$\begin{cases} P_{el,t}^{in} = m_{el,t}^{out} + H_{el,t}^{xs} + H_{el,t}^{loss}, \\ m_{d,j,t}^{out} = \lambda_{el,t} P_{el,t}^{in} \zeta_{el}, \end{cases} \quad (3)$$

where  $P_{el,t}^{in}$  is the electrical power consumed by the electrolytic cell;  $m_{d,j,t}^{out}$  and  $\lambda_{el,t}$  are the quality and efficiency of hydrogen gas produced by the electrolytic cell, respectively;  $H_{el,t}^{xs}$  and  $H_{el,t}^{loss}$  refer to the thermal energy generated during the operation of the electrolytic cell and the heat dissipation loss, respectively; and  $\zeta_{el}$  is the conversion coefficient of the electrolytic cell.

Under constant temperature and pressure conditions, the hydrogen production efficiency of the electrolytic cell is related to the current efficiency and voltage efficiency, as shown in Eq. 4:

$$\begin{cases} \lambda_{el,t} = \lambda_{el,t}^I \lambda_{el,t}^U, \\ \lambda_{el,t}^I = 96.5e^{\left(\frac{-746}{I_{el,t}^U}\right)}, \\ \lambda_{el,t}^U = \frac{U_{el,t}^{zx}}{U_{el,t}^{dj}}, \end{cases} \quad (4)$$

where  $\lambda_{el,t}^I$  and  $\lambda_{el,t}^U$  represent the current efficiency and voltage efficiency of the electrolytic cell, respectively;  $I_{el,t}^U$  is the operating current of the electrolytic cell;  $U_{el,t}^{zx}$  is the thermal neutral voltage; and  $U_{el,t}^{dj}$  is the voltage of electrolysis of water.

Under certain temperature and pressure conditions, the electrolysis of water voltage of the electrolytic cell depends on the current density, as shown in Eq. 5:

$$\begin{cases} U_{el,t}^{dj} = U_{el,t}^{rev}(T, P) + U_{el,t}^{ohm}(j, T) + U_{el,t}^{h2}(j, T) + U_{el,t}^{o2}(j, T), \\ U_{el,t}^{rev}(T, P) = 1.5184 - 1.5421 \times 10^{-3}T + 9.523 \times 10^{-5}T^2e + 9.84 \times 10^{-8}T^2, \\ U_{el,t}^{ohm} = I_{el,t} R_{el}, \\ U_{el,t}^{h2} = \frac{ET}{\vartheta_1 n_1 Y} \ln \frac{j}{j_1}, \\ U_{el,t}^{o2} = \frac{ET}{\vartheta_2 n_2 Y} \ln \frac{j}{j_2}, \end{cases} \quad (5)$$

where  $U_{el,t}^{rev}$ ,  $U_{el,t}^{ohm}$ ,  $U_{el,t}^{h2}$ , and  $U_{el,t}^{o2}$  refer to reversible voltage, resistance voltage drop, hydrogen overpotential, and oxygen overpotential, respectively;  $T$ ,  $P$ , and  $j$  represent temperature, pressure, and current density, respectively;  $R_{el}$  is the resistance of the electrolyte;  $E$  and  $Y$  are universal gas and Faraday constant, respectively;  $\vartheta_1$ ,  $n_1$ , and  $j_1$  are the charge transfer coefficient, electron transfer number, and current density of the cathode,

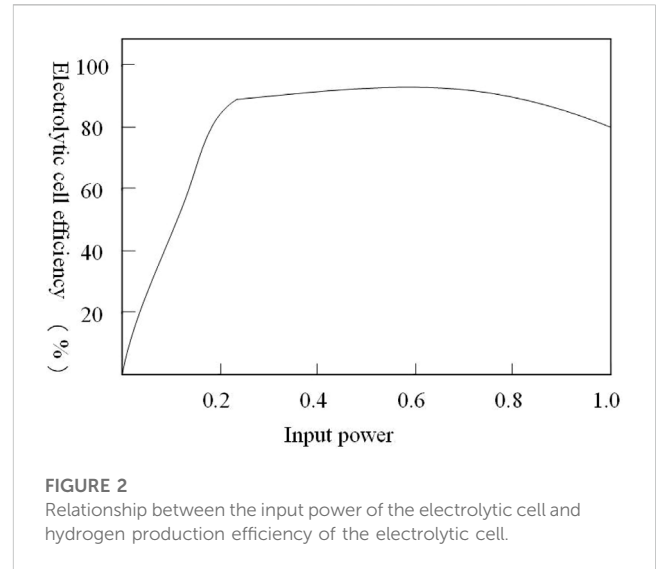


FIGURE 2 Relationship between the input power of the electrolytic cell and hydrogen production efficiency of the electrolytic cell.

respectively;  $\vartheta_2$ ,  $n_2$ , and  $j_2$  are the charge transfer coefficient, electron transfer number, and current density of the anode.

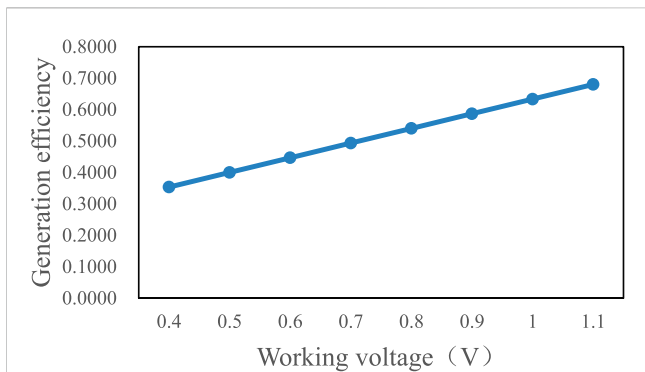
Referring to the relevant parameters of the electrolytic cell in Liu et al. (2022), the non-linear relationship between the input power of the electrolytic cell and the hydrogen production efficiency of the electrolytic cell is shown in Figure 2. The electrolysis cell has the highest hydrogen production efficiency when the input power accounts for approximately 20% of the rated power; however, the hydrogen production amount is small. The optimal operating range is (50%, 100%) of the rated power.

### 3.1.4 Hydrogen storage tank

Based on different pressure requirements, hydrogen storage tanks mainly involve three types of hydrogen storage methods: solid, liquid, and gaseous. Among them, high-pressure hydrogen storage in the gaseous state has been the most widely used, mature, and low-cost method, with a pressure of up to 20 MPa. When the pressure is less than 10 MPa, the ideal equation of state can be used to build the relationship between the mass and pressure of the hydrogen storage tank. However, due to the small relative molecular weight of hydrogen, when the pressure exceeds 10 MPa, it is easy to lead to explosion. At this time, the ideal equation of state does not accurately describe the relationship between mass and pressure. Fan's equation can characterize the mass and pressure of hydrogen storage tanks by considering the repulsive and gravitational forces between molecules, as shown in Eq. 6:

$$\begin{cases} \left( p_{EHS,t} + c_1 \left( \frac{n_{EHS,t}}{V_{EHS,t}} \right)^2 \right) (V_{EHS,t} - c_2 n_{EHS,t}) = n_{EHS,t} \cdot a \cdot T_H, \\ m_{EHS,t} = M_H \cdot n_{EHS,t}, \end{cases} \quad (6)$$

where  $p_{EHS,t}$  is the pressure of the hydrogen storage tank at time  $t$ ;  $c_1$  and  $c_2$  are Fan's coefficients;  $n_{EHS,t}$  is the amount of hydrogen in the hydrogen storage tank;  $V_{EHS,t}$  is the volume of the hydrogen storage tank;  $a$  is a constant;  $T_H$  is the temperature of hydrogen gas; and  $M_H$  is the relative molecular weight of hydrogen gas.



**FIGURE 3**  
Relationship between fuel cell power generation and voltage.

According to Eq. 5, the relationship between the pressure and mass of the hydrogen storage tank is shown in Eq. 7:

$$P_{EHS,t} = \frac{m_{EHS,t} \cdot a \cdot T_H}{M_H V_{EHS,t} - c_2 m_{EHS,t}} - c_1 \left( \frac{m_{EHS,t}}{M_H V_{EHS,t}} \right)^2 \quad (7)$$

The capacity of the hydrogen storage tank is shown in Eq. 8:

$$m_{EHS,t+1} = m_{EHS,t} + m_{EHS,t}^{in} - m_{EHS,t}^{out} \quad (8)$$

where  $m_{EHS,t+1}$  is the hydrogen mass of the hydrogen storage tank at time  $t+1$ ;  $m_{EHS,t}^{in}$  is the hydrogen mass of the hydrogen storage tank at time  $t$ ; and  $m_{EHS,t}^{out}$  is the hydrogen release amount of the hydrogen storage tank at time  $t$ .

### 3.1.5 Hydrogen fuel cell

The hydrogen fuel cell can be regarded as the reverse reaction of electrolyzed water, and its energy model is shown in Eq. 9:

$$\begin{cases} m_{hf,t} = P_{hf,t} + H_{hf,t}^{cr} + H_{hf,t}^{loss}, \\ P_{hf,t} = \lambda_{hf,t} m_{hf,t} \zeta_{hf}, \\ \lambda_{hf,t} = \frac{2V_{hf}}{\Delta H_{h_2}}, \end{cases} \quad (9)$$

where  $m_{hf,t}$  is the hydrogen consumed by the hydrogen fuel cell;  $P_{hf,t}$  and  $H_{hf,t}^{cr}$  are the electric energy and thermal energy generated by the hydrogen fuel cell, respectively;  $H_{hf,t}^{loss}$  is the heat energy lost by the hydrogen fuel cell;  $\lambda_{hf,t}$  is the electrical efficiency of the hydrogen fuel cell;  $V_{hf}$  is the operating voltage of the hydrogen fuel cell;  $\Delta H_{h_2}$  is the enthalpy value of hydrogen gas; and  $\zeta_{hf}$  is the conversion coefficient of the hydrogen fuel cell. The relationship between fuel cell power generation and voltage is shown in Figure 3.

### 3.1.6 Electric heat transfer equipment

Electric heat transfer equipment converts electrical energy into thermal energy through consumption, and its conversion model is specifically shown in Eq. 10:

$$H_{EH,t} = \lambda_{EH,t} P_{EH,t}, \quad (10)$$

where  $H_{EH,t}$  is the thermal energy generated by the electric heat transfer equipment at time  $t$ ;  $\lambda_{EH,t}$  is the conversion efficiency of the electric heat transfer equipment; and  $P_{EH,t}$  is the electrical energy consumed by the electric heat transfer equipment.

## 3.2 Analysis of system uncertainty and response characteristics

This section analyzes the uncertainties faced by distributed hydrogen systems and the response characteristics of various pieces of equipment in the system, laying the foundation for constructing a multi-timescale operation optimization model in Section 4.

### 3.2.1 Wind and photovoltaic power generation units

In terms of response characteristics, wind and photovoltaic power generation units can quickly abandon wind and light when they exceed the maximum output value, and their adjustability is strong. The response time of the distributed electric hydrogen coupling system for wind and solar power generation units is short, and the response timescale is set to  $\tau_1$ . In terms of uncertainty, wind and solar power have high output uncertainty due to the influence of geographical location, environmental temperature, light intensity, and wind speed. Based on this, Bai et al. (2021) used a combination of clustering and particle swarm optimization algorithms to determine n typical wind and solar output scene sets and weighted and stacked n output scenes and further used the uncertainty set of wind and solar output to represent the uncertainty of wind and solar output, as shown in Eqs 11, 12:

$$\begin{cases} G_{P_{wind,t}} = \{ \tilde{P}_{wind,t}^D = (\tilde{P}_{wind,1}^D, \tilde{P}_{wind,2}^D, \dots, \tilde{P}_{wind,T}^D), \forall t = 1, 2, \dots, T \}, \\ P_{wind,t}^{D,\min} \leq \tilde{P}_{wind,t}^D \leq P_{wind,t}^{D,\max}, \\ \sum_{t=1}^T \left| \frac{2\tilde{P}_{wind,t}^D - (P_{wind,t}^{D,\min} + P_{wind,t}^{D,\max})}{P_{wind,t}^{D,\min} + P_{wind,t}^{D,\max}} \right| \leq \eta_{wind}, \end{cases} \quad (11)$$

$$\begin{cases} G_{P_{pv,t}} = \{ \tilde{P}_{pv,t}^D = (\tilde{P}_{pv,1}^D, \tilde{P}_{pv,2}^D, \dots, \tilde{P}_{pv,T}^D), \forall t = 1, 2, \dots, T \}, \\ P_{pv,t}^{D,\min} \leq \tilde{P}_{pv,t}^D \leq P_{pv,t}^{D,\max}, \\ \sum_{t=1}^T \left| \frac{2\tilde{P}_{pv,t}^D - (P_{pv,t}^{D,\min} + P_{pv,t}^{D,\max})}{P_{pv,t}^{D,\min} + P_{pv,t}^{D,\max}} \right| \leq \eta_{pv}, \end{cases} \quad (12)$$

where  $G_{P_{wind,t}}$  is the uncertainty set of wind power generation;  $\tilde{P}_{wind,t}^D$  is the actual output of wind power generation at time  $t$ ;  $P_{wind,t}^{D,\min}$  and  $P_{wind,t}^{D,\max}$  are the upper and lower limits of wind power generation, respectively;  $\eta_{wind}$  is the robustness factor for the uncertainty set of wind power generation;  $G_{P_{pv,t}}$  is the uncertainty set of photovoltaic power generation;  $\tilde{P}_{pv,t}^D$  is the actual output of photovoltaic power generation at time  $t$ ;  $P_{pv,t}^{D,\min}$  and  $P_{pv,t}^{D,\max}$  are the upper and lower limits of photovoltaic power generation, respectively; and  $\eta_{pv}$  is the robustness factor for the uncertainty set of photovoltaic power generation.

### 3.2.2 Wind and photovoltaic power generation units

The coupling unit mainly includes electrolytic cell, hydrogen fuel cell, electric heat transfer equipment, and hydrogen storage tank equipment. In terms of response characteristics, the response time of coupling equipment such as electrolytic cells



and electric heat-transfer equipment is longer than that of wind and solar power generation units. The alkaline electrolytic cell has a fast start and stop speed, with a dynamic response time of approximately 10 min, which is slower than that of wind and solar power generation units. The dynamic response timescale is set to  $\tau_2$ . The response speed of electric heat-transfer equipment is equivalent to that of electrolytic cells, and its dynamic response timescale is  $\tau_2$ . The dynamic response time of the hydrogen fuel cell is equivalent to that of the alkaline electrolyzer, and the dynamic response timescale is  $\tau_2$ . The hydrogen storage tank has the advantage of fast adjustment, and its dynamic response timescale is between the wind and solar power generation unit and the electrolytic cell, with a dynamic response timescale of  $\tau_3$ . For the uncertainty analysis of coupled units, due to the control feedback system inside the coupled units, the overall conversion output is relatively stable, so its uncertainty is not considered temporarily.

### 3.2.3 Wind and photovoltaic power generation units

The distributed electric hydrogen coupling system constructed in this article mainly includes three types: electrical load, thermal load, and hydrogen load. In terms of response characteristics, it is mainly scheduled through demand response. It is divided into three categories based on the length of the response timescale: the first type is a long-term demand response, including food processing industry and long-term electric heating, which is not flexible enough and requires scheduling and planning 1 day in advance. The dynamic response timescale is set to  $\tau_4$ . The second type is demand response with a short timescale, including short-term electric heating, which is consistent with the response timescale of alkaline electrolytic cells as  $\tau_2$ . The third type is demand response at an ultrashort timescale, including electric irrigation, which is consistent with the response timescale of  $\tau_1$  in the wind and solar power generation unit.

The uncertainty analysis of load demand is mainly influenced by user subjectivity and energy prices, and its uncertainty is characterized by the load deviation rate, as shown in Eqs 13–15:

$$[L_{ele,t}]^\pm = [\bar{L}_{ele,t}(1 - \varepsilon_{ele}), \bar{L}_{ele,t}(1 + \varepsilon_{ele})], \quad (13)$$

$$[L_{heat,t}]^\pm = [\bar{L}_{heat,t}(1 - \varepsilon_{heat}), \bar{L}_{heat,t}(1 + \varepsilon_{heat})], \quad (14)$$

$$[L_{hy,t}]^\pm = [\bar{L}_{hy,t}(1 - \varepsilon_{hy}), \bar{L}_{hy,t}(1 + \varepsilon_{hy})], \quad (15)$$

where  $[L_{ele,t}]^\pm$ ,  $[L_{heat,t}]^\pm$ , and  $[L_{hy,t}]^\pm$  are the demand intervals for electrical load, thermal load, and hydrogen load at time  $t$ , respectively;  $\bar{L}_{ele,t}$ ,  $\bar{L}_{heat,t}$ , and  $\bar{L}_{hy,t}$  are the expected electrical load, thermal load, and hydrogen load at time  $t$ , respectively; and  $\varepsilon_{ele}$ ,  $\varepsilon_{heat}$ , and  $\varepsilon_{hy}$  are the expected deviation rates between electrical load, thermal load, and hydrogen load, respectively.

The response timescales of different call outputs and loads are summarized in Eq. 16:

$$\begin{cases} \text{Long timescale: } L_{PDR,\tau_4}^1, \\ \text{Short timescale: } L_{PDR,\tau_2}^1, m_{dj,\tau_2}^{out}, P_{hf,\tau_2}, H_{EH,\tau_2}, m_{EHS,\tau_3}, \\ \text{Ultra short timescale: } L_{PDR,\tau_1}^1, P_{wind,\tau_1}, P_{pv,\tau_1}, P_{hf,\tau_1}. \end{cases} \quad (16)$$

## 4 Optimization model for multi-timescale operation of the electric hydrogen coupling system

### 4.1 Operational optimization ideas

Based on the analysis results of response characteristics of different pieces of equipment in Section 3.2 of the system, it can be seen that due to the coupling of distributed power supply, hydrogen network, and thermal network, the output characteristics of each type of energy unit are different, resulting in different scheduling response times for each part. Therefore, this paper depends on day-ahead-day-in-real-time rolling optimization for optimization design. In the day-ahead stage, determine the start and stop operation plans for each unit, and in the day-in stage, determine the adjustment plans for each unit based on the errors between the wind and solar output and load demand in the day ahead and day in stages. In the real-time stage, the adjustment plan for each unit is determined based on the error between the daily and real-time stages of wind and solar output and load demand. The optimization design concept is shown in Figure 4:

Plan development should be carried out 1 day in advance, i.e., 24 h in advance, with a scheduling timescale of  $\tau_4$ . In the day-ahead phase, based on the forecast results of wind and solar power and various loads, the startup and shutdown plans and output plans of electrolyzer, hydrogen storage tank, hydrogen fuel cell, and electric-to-heat equipment in the system are determined with the minimum initial operating cost of the system, and the first type of a long-term demand response scheduling plan is formulated.

In the day-in rolling optimization stage, the scheduling period is 4 h. In order to coordinate the response timescale between the hydrogen storage tank and other coupling equipment, the scheduling timescale is selected as the least common multiples of  $\tau_2$  and  $\tau_3$  and set to  $\xi$ . At the same time, according to the deviation between the wind power and load forecast and the day-ahead forecast results in the rolling optimization, taking into account the flexibility of response, the demand response scheduling of the second type of timescale is mainly used, supplemented by the deviation adjustment of the hydrogen storage tank electrolyzer and hydrogen fuel cell. The rolling optimization goal at this stage is to minimize the cost of deviation adjustment.

In the real-time rolling optimization stage, the scheduling cycle is 15 min, and the scheduling timescale is  $\tau_1$ . This stage is based on the deviation between the predicted results of real-time rolling optimization for wind and solar power, load forecasting, and intraday rolling optimization. The adjustment is mainly based on the third type of demand response. If it is insufficient, it is adjusted by interacting with the external network to purchase or sell electricity. At this stage, the rolling optimization goal is also to minimize the deviation adjustment cost.

### 4.2 Day-ahead optimization model

#### 4.2.1 Objective function

In the current optimization stage, the distributed electric hydrogen coupling system aims to minimize the total operating cost of the coupling system as the objective function. The operating costs of the previous stage include the start-up and shutdown costs of the unit, the

operating costs of the unit, the demand response call costs, the external network interaction costs, and the uncertainty costs caused by multiple uncertainties in the system, as shown in Eq. 17:

$$\begin{cases} C_{total}^{rq} = C_{total}^{rp-qt} + C_{total}^{rq-yx} + C_{total}^{rq-dr} + C_{total}^{rq-jh} + C_{total}^{rq-un}, \\ C_{total}^{rp-qt} = \sum u_i \theta_i \quad i \in \{pv, wind, dj, EHS, hf, EH\}, \\ C_{total}^{rq-yx} = \sum_{t=1}^{24} \left( P_{wind,t}^{rq} P_{wind} + P_{pv,t}^{rq} P_{pv} + m_{dj,t}^{rq-out} P_{dj} + P_{hf,t}^{rq} P_{hf} + \left( m_{EHS,t}^{rq-in} + m_{EHS,t}^{rq-out} \right) P_{EHS} + H_{EH,t}^{rq} P_{EH} \right), \\ C_{total}^{rq-dr} = \sum_{t=1}^{24} L_{PDR,t}^1 P_{PDR}^1, \\ C_{total}^{rq-jh} = \sum_{t=1}^{24} \left( P_{buy,t}^{rq-jh} P_{buy} - P_{sale,t}^{rq-jh} P_{sale} \right), \\ C_{total}^{rq-un} = \sum_{t=1}^{24} v_{pun} \left( P_{wind,t}^{rq} \eta_{wind}^{rq} + P_{pv,t}^{rq} \eta_{pv}^{rq} + m_{dj,t}^{rq-out} \varepsilon_{cl} + P_{hf,t}^{rq} \varepsilon_{hf} \right), \\ \end{cases} \quad (17)$$

where  $C_{total}^{rq}$  is the total operating cost of the distributed electric hydrogen coupling system in the day-ahead stage;  $C_{total}^{rp-qt}$ ,  $C_{total}^{rq-yx}$ ,  $C_{total}^{rq-dr}$ ,  $C_{total}^{rq-jh}$ , and  $C_{total}^{rq-un}$  refer to the operating costs of the distributed electric hydrogen coupling system in the early stage, including the start-up and shutdown costs of the unit, the operating costs of the unit, the demand response call costs, the external network interaction costs, and the uncertainty costs caused by multiple uncertainties in the system, respectively;  $u_i$  is the start-up and shutdown costs of unit  $i$ ;  $\theta_i = 1$  represents the start of the unit, otherwise the unit will not start;  $P_{wind,t}^{rq}$ ,  $P_{pv,t}^{rq}$ ,  $m_{dj,t}^{rq-out}$ ,  $P_{hf,t}^{rq}$ , and  $H_{EH,t}^{rq}$  are the output plan of wind turbine generator set, photovoltaic generator set, electrolytic cell, hydrogen fuel cell, and electricity-to-heat equipment at time  $t$  in the day-ahead stage, respectively;  $m_{EHS,t}^{rq-in}$  and  $m_{EHS,t}^{rq-out}$  are the hydrogen storage and release capacities of the hydrogen storage tank at time  $t$ , respectively;  $P_{wind}$ ,  $P_{pv}$ ,  $P_{dj}$ ,  $P_{hf}$ ,  $P_{EHS}$ , and  $P_{EH}$  are the unit operating costs of wind turbine generator set, photovoltaic generator set, electrolytic cell, hydrogen fuel cell, hydrogen storage tank, and electric heat-transfer equipment, respectively;  $P_{PDR}^1$  is the first type of demand response unit scheduling cost;  $P_{buy,t}^{rq-jh}$  and  $P_{sale,t}^{rq-jh}$  represent the purchased and sold electricity of the distributed electric hydrogen coupling system when interacting with the external network at time  $t$ , respectively;  $p_{buy}$  and  $p_{sale}$  are the unit electricity purchase and unit electricity sale costs when the distributed electric hydrogen coupling system interacts with the external network, respectively; and  $v_{pun}$  is the unit uncertainty cost.

### 4.2.2 Constraint condition

The constraints of the distributed electric hydrogen coupling system in the early stage include power balance constraints and equipment operation constraints. The power balance constraints mainly include electrical energy balance, thermal energy balance, and hydrogen energy balance, as shown in Eq. 18:

$$\begin{cases} P_{wind,t}^{rq} + P_{pv,t}^{rq} + P_{hf,t}^{rq-jh} + P_{hf,t}^{rq} + L_{PDR,t}^1 = I_{ele,t}^{rq} + P_{el,t}^{rq-in} + P_{sale,t}^{rq-jh}, \\ H_{EH,t}^{rq} + t + H_{hf,t}^{rq-cr} + H_{dj,t}^{rq-cr} = L_{heat,t}^{rq}, \\ m_{EHS,t}^{rq-out} + m_{dj,t}^{rq-out} = m_{hf,t}^{rq} + L_{hy,t} + m_{EHS,t}^{rq-in}, \\ \end{cases} \quad (18)$$

Equipment operation constraints mainly include wind and solar power unit operation constraints, coupled unit operation constraints, and demand response constraints, as shown in Eq. 19:

$$\begin{cases} P_i^{min} \leq P_{i,t}^{rq} \leq P_i^{max}, \quad i = hf, \\ \Delta P_i^{min} \leq P_{i,t+1}^{rq} - P_{i,t}^{rq} \leq \Delta P_i^{max}, \quad i = hf, \\ H_{EH}^{min} \leq H_{EH,t}^{rq}, \quad t \leq H_{EH}^{max}, \\ \Delta H_{EH}^{min} \leq H_{EH,t+1}^{rq} - H_{EH,t}^{rq}, \quad t \leq \Delta H_{EH}^{max}, \\ m_{EHS}^{min} \leq m_{EHS,t} \leq m_{EHS}^{max}, \\ \begin{cases} m_{dj}^{min} \leq m_{dj,t}^{rq-out} \leq m_{dj}^{max}, \\ \Delta m_{dj}^{min} \leq m_{dj,t+1}^{rq-out} - m_{dj,t}^{rq-out} \leq \Delta m_{dj}^{max}, \end{cases} \\ L_{PDR,t}^{min,1} \leq L_{PDR,t}^1 \leq L_{PDR,t}^{max,1}, \\ \end{cases} \quad (19)$$

where  $P_i^{min}$  and  $P_i^{max}$  are the minimum and maximum output of unit  $i$ ;  $\Delta P_i^{min}$  and  $\Delta P_i^{max}$  are the minimum and maximum values for unit  $i$  to climb the slope;  $H_{EH}^{min}$  and  $H_{EH}^{max}$  are the minimum and maximum output of the electric heat-transfer equipment;  $\Delta H_{EH}^{min}$  and  $\Delta H_{EH}^{max}$  are the minimum and maximum values for the climbing of the electric heat transfer equipment;  $m_{EHS}^{min}$  and  $m_{EHS}^{max}$  are the minimum and maximum hydrogen storage capacities of the hydrogen storage tank;  $m_{dj}^{min}$  and  $m_{dj}^{max}$  are the minimum and maximum output of the electrolytic cell;  $\Delta m_{dj}^{min}$  and  $\Delta m_{dj}^{max}$  are the minimum and maximum values for climbing the electrolytic cell slope; and  $L_{PDR,t}^{min,1}$  and  $L_{PDR,t}^{max,1}$  are the minimum and maximum scheduling amount for the first type of demand response, respectively.

## 4.3 Day-in rolling optimization model

### 4.3.1 Objective function

In the day-in rolling optimization stage, based on the day-ahead scheduling plan, the scheduling of the second type of demand response and the output adjustment of coupled units are carried out. The optimization goal of the day-in rolling stage is to minimize the adjustment cost, as shown in Eq. 20:

$$\begin{cases} \min C_{total}^{rn} = \min \left( C_{total}^{rn-dr} + \Delta C_{total}^{rn-dj} \theta_i^{tz} + \Delta C_{total}^{rn-hf} \theta_{hf}^{tz} + \Delta C_{total}^{rn-EH} \theta_{EH}^{tz} + \Delta C_{total}^{rn-EHS} \theta_{EHS}^{tz} \right), \\ \Delta C_{total}^{rn-dr} = \sum_{t=1}^{24} \sum_{s=1}^4 L_{PDR,ts}^2 P_{PDR}^2, \\ \Delta C_{total}^{rn-dj} = \sum_{t=1}^{24} \sum_{s=1}^4 \Delta m_{dj,ts}^{rn} u_{dj}^{rn-tz}, \\ \Delta C_{total}^{rn-hf} = \sum_{t=1}^{24} \sum_{s=1}^4 \Delta P_{hf,ts}^{rn} u_{hf}^{rn-tz}, \\ \Delta C_{total}^{rn-EH} = \sum_{t=1}^{24} \sum_{s=1}^4 \Delta H_{EH,t}^{rn} t s u_{EH}^{rn-tz}, \\ \Delta C_{total}^{rn-EHS} = \sum_{t=1}^{24} \sum_{s=1}^4 \left( \Delta m_{EHS,ts}^{rn-out} u_{EHS}^{rn-tz} + \Delta m_{EHS,ts}^{rn-in} u_{EHS}^{rn-tz} \right), \\ \end{cases} \quad (20)$$

where  $C_{total}^{rn-dr}$  is the scheduling cost for the second type of demand response in the day-in stage;  $\Delta C_{total}^{rn-i}$  is the adjustment cost for the  $i$ th unit during the day-in stage,  $i \in \{dj, hf, EH, EHS\}$ ;  $\theta_i^{tz}$  is a Boolean variable,  $\theta_i^{tz} = 1$ , indicating that unit  $i$  participates in the intraday adjustment, otherwise it will not participate;  $L_{PDR,ts}^2$  and  $P_{PDR}^2$  are the scheduling quantity and unit scheduling cost for the second type of

demand response, respectively;  $\Delta m_{d,j,t,s}^{rn}$ ,  $\Delta P_{h,f,t,s}^{rn}$ , and  $\Delta H_{EH,t,s}^{rn}$  are the adjustment amounts of electrolytic cell, hydrogen fuel cell, and electric heat-transfer equipment in the day-in stage, respectively;  $u_{d,j}^{rn-tz}$ ,  $u_{h,f}^{rn-tz}$ , and  $u_{EH}^{rn-tz}$  are the unit adjustment costs of electrolytic cell, hydrogen fuel cell, and electric-to-heat equipment in the day stage, respectively;  $\Delta m_{EHS,t,s}^{rn-out}$  and  $\Delta m_{EHS,t,s}^{rn-in}$  are the hydrogen release and storage adjustment amount of the hydrogen storage tank, respectively; and  $u_{EHS}^{rn-tz}$  represents the unit adjusted cost of the hydrogen storage tank.

### 4.3.2 Constraint condition

The constraints in the day-in stage also include power balance constraints and equipment operation constraints. The power balance constraints are shown in Eq. 21, and the equipment operation constraints are in the same form as Eq. 19.

$$\left\{ \begin{aligned} & \sum_{s=1}^{\frac{4}{\xi}} (P_{wind,t,s}^{rn} + P_{pv,t,s}^{rn} + P_{h,f,t,s}^{rn} + L_{PDR,t,s}^1 + L_{PDR,t,s}^2) + P_{buy,t}^{rq-jh} \\ &= \sum_{s=1}^{\frac{4}{\xi}} (\Delta P_{el,t,s}^{rn-in} + L_{ele,t,s}^{rn}) + P_{el,t}^{rq-in} + P_{sale,t}^{rq-jh}, \\ & H_{EH,t}^{rq} + t + \sum_{s=1}^{\frac{4}{\xi}} (\Delta H_{EH,t,s}^{rn} + H_{h,f,t,s}^{rq-cr} + \Delta H_{h,f,t,s}^{rn-cr} + H_{d,j,t,s}^{rq-cr} + \Delta H_{d,j,t,s}^{rn-cr}) \\ &= \sum_{s=1}^{\frac{4}{\xi}} (L_{heat,t,s}^{rn}), \\ & m_{EHS,t}^{rq-out} + m_{d,j,t}^{rq-out} + \sum_{s=1}^{\frac{4}{\xi}} (\Delta m_{EHS,t,s}^{rn-out} + \Delta m_{d,j,t,s}^{rn-out}) \\ &= \sum_{s=1}^{\frac{4}{\xi}} (\Delta m_{h,f,t,s}^{rn} + L_{hy,t,s}^{rn} + \Delta m_{EHS,t,s}^{rn-in}) + m_{h,f,t}^{rq} + m_{EHS,t}^{rq-in}. \end{aligned} \right. \tag{21}$$

## 4.4 Real-time optimization model

### 4.4.1 Objective function

In the real-time optimization stage, based on the daily rolling optimization plan, the third type of demand response and hydrogen fuel cell output adjustment are carried out. The optimization goal of the real-time rolling stage is to minimize the adjustment cost  $\Delta C_{total}^{ss}$  as shown in Eq. 22:

$$\left\{ \begin{aligned} & \min \Delta C_{total}^{ss} = \min (\Delta C_{total}^{ss-dr} + \Delta C_{total}^{ss-hf} \theta_{hf}^{ss-tz} + \Delta C_{total}^{ss-jh} \theta_{jh}^{ss-tz}), \\ & \Delta C_{total}^{ss-dr} = \sum_{t=1}^{\frac{24}{\tau_4}} \sum_{s=1}^{\frac{4}{\xi}} \sum_{y=1}^{\frac{15}{\tau_1}} I_{PDR,t,s,y}^3 P_{PDR}^3, \\ & \Delta C_{total}^{ss-hf} = \sum_{t=1}^{\frac{24}{\tau_4}} \sum_{s=1}^{\frac{4}{\xi}} \sum_{y=1}^{\frac{15}{\tau_1}} \Delta P_{h,f,t,s,y}^{ss} u_{h,f}^{ss-tz}, \\ & \Delta C_{total}^{ss-jh} = \sum_{t=1}^{\frac{24}{\tau_4}} \sum_{s=1}^{\frac{4}{\xi}} \sum_{y=1}^{\frac{15}{\tau_1}} (\Delta P_{buy,t,s,y}^{ss-jh} P_{buy} - \Delta P_{sale,t,s,y}^{ss-jh} P_{sale}), \end{aligned} \right. \tag{22}$$

where  $\Delta C_{total}^{ss-dr}$  is the scheduling cost for the third type of demand response in the real-time phase;  $\Delta C_{total}^{ss-hf}$  is the adjustment cost of the hydrogen fuel cell in the real-time phase;  $\Delta C_{total}^{ss-jh}$  is the cost of interaction between the real-time distributed electric hydrogen

coupling system and the external network;  $\theta_{hf}^{ss-tz}$  is a Boolean variable, and  $\theta_{hf}^{ss-tz} = 1$  is the output of the hydrogen fuel cell adjusted in the real-time phase, otherwise it will not be adjusted;  $\theta_{jh}^{ss-tz}$  is also a Boolean variable, where  $\theta_{jh}^{ss-tz} = 1$  indicates correction and adjustment through external network interaction, otherwise the opposite is true;  $L_{PDR,t,s,y}^3$  and  $P_{PDR}^3$  are the scheduling quantity and unit scheduling cost for the third type of demand response, respectively;  $\Delta P_{h,f,t,s,y}^{ss}$  and  $u_{h,f}^{ss-tz}$  are the adjustment amount and unit adjustment cost of the hydrogen fuel cell in the real-time phase, respectively;  $\Delta P_{buy,t,s,y}^{ss-jh}$  and  $\Delta P_{sale,t,s,y}^{ss-jh}$  refer to the purchase and sale of electricity during the real-time phase and external network adjustment, respectively.

### 4.4.2 Constraint condition

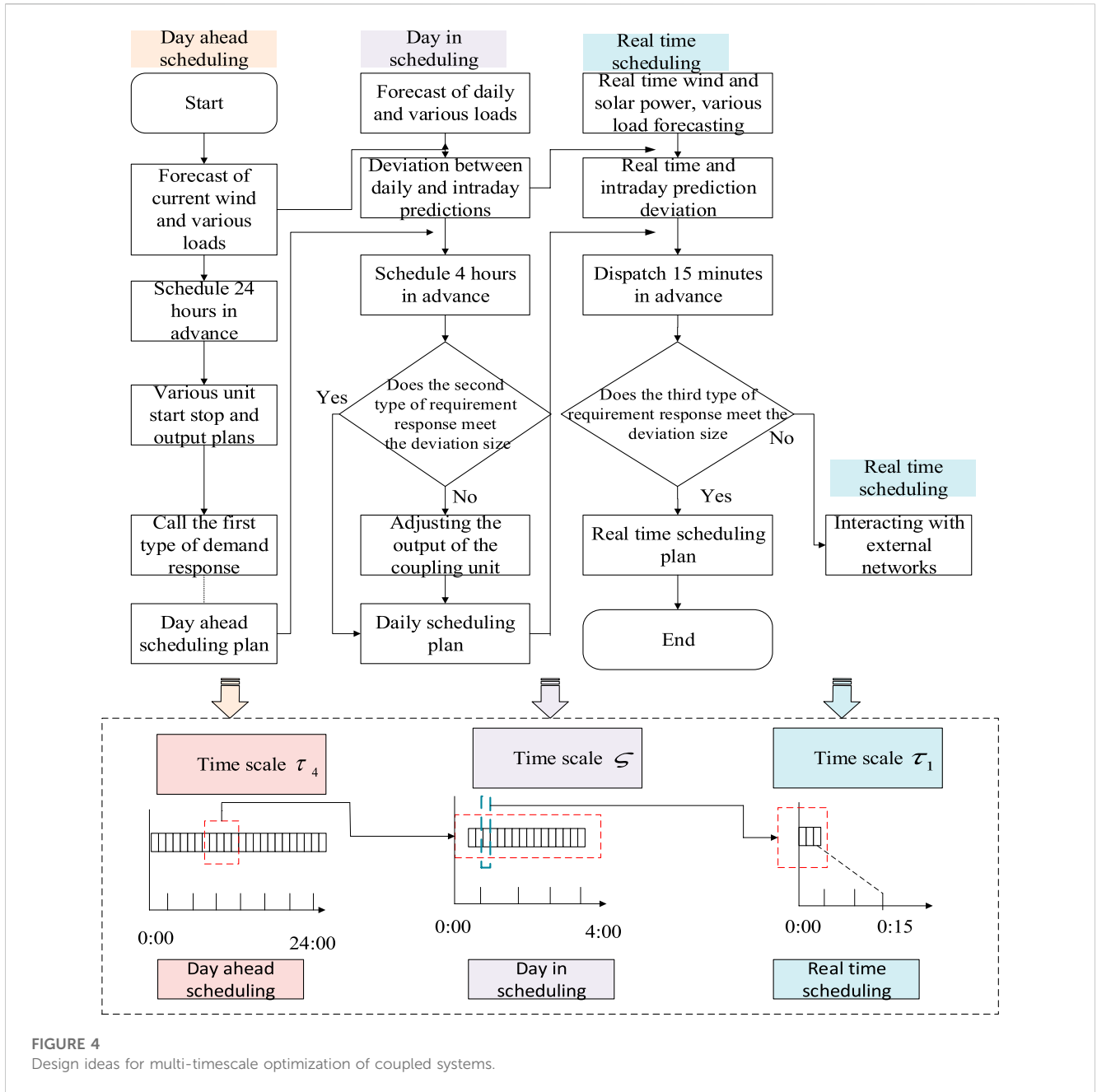
The system balance constraints in the real-time phase are the same as Eq. 18, and the equipment operation constraints are shown in Eq. 23:

$$\left\{ \begin{aligned} & \sum_{s=1}^{\frac{4}{\xi}} (P_{wind,t,s}^{rn} + P_{pv,t,s}^{rn} + L_{PDR,t,s}^1 + L_{PDR,t,s}^2) + P_{buy,t}^{rq-jh} \\ &+ \sum_{s=1}^{\frac{4}{\xi}} \sum_{y=1}^{\frac{15}{\tau_1}} (\Delta P_{buy,t,s,y}^{ss-jh} + P_{h,f,t,s}^{rn}) = \sum_{s=1}^{\frac{4}{\xi}} (\Delta P_{el,t,s}^{rn-in}) \\ &+ \sum_{s=1}^{\frac{4}{\xi}} \sum_{y=1}^{\frac{15}{\tau_1}} (L_{ele,t,s,y}^{ss} + \Delta P_{sale,t,s,y}^{ss-jh}) + P_{el,t}^{rq-in} + P_{sale,t}^{rq-jh}, \\ & H_{EH,t}^{rq} + t + \sum_{s=1}^{\frac{4}{\xi}} (\Delta H_{EH,t,s}^{rn} + H_{h,f,t,s}^{rq-cr} + \Delta H_{h,f,t,s}^{rn-cr} + H_{d,j,t,s}^{rq-cr} + \Delta H_{d,j,t,s}^{rn-cr}) \\ &+ \sum_{s=1}^{\frac{4}{\xi}} \sum_{y=1}^{\frac{15}{\tau_1}} (\Delta H_{h,f,t,s,y}^{rn-cr}) = \sum_{s=1}^{\frac{4}{\xi}} \sum_{y=1}^{\frac{15}{\tau_1}} (L_{heat,t,s,y}^{rn}), \\ & m_{EHS,t}^{rq-out} + m_{d,j,t}^{rq-out} + \sum_{s=1}^{\frac{4}{\xi}} (\Delta m_{EHS,t,s}^{rn-out} + \Delta m_{d,j,t,s}^{rn-out}) \\ &= \sum_{s=1}^{\frac{4}{\xi}} (\Delta m_{h,f,t,s}^{rn} + L_{hy,t,s}^{ss} + \Delta m_{EHS,t,s}^{rn-in}) + m_{h,f,t}^{rq} + m_{EHS,t}^{rq-in}. \end{aligned} \right. \tag{23}$$

## 4.5 Model solution

The multi-timescale optimization model of the distributed electro-hydrogen coupling system is a complex uncertain mixed integer non-linear programming problem, and the methods for solving uncertainty mainly include approximation and decomposition methods. The decomposition method includes the Benders decomposition algorithm and column-and-constraint-generation algorithm (C&CG). Due to the fact that the C&CG algorithm considers the constraints and variables of the subproblem compared to the Benders decomposition algorithm, which can accelerate convergence, this section adopts the C&CG algorithm for solution. The C&CG algorithm iteratively converges the main problem and subproblems to solve. The main problem is the optimal solution that satisfies the conditions under a known finite distribution, providing a lower bound (LB) value for the robust optimization model. The subproblem is to seek the worst-case distribution and provide an upper bound (UB) value for the robust optimization model under the given conditions of the decision variables in the first stage. The specific model of the C&CG algorithm is referenced in Song et al. (2023), and Cplex is further used for solution.





## 5 Example analysis

### 5.1 Basic data

Multiple demonstration projects for electric hydrogen coupling have been put into operation in a certain province of China, with rich experience in electric hydrogen coupling systems. Therefore, in order to verify the effectiveness of the model, a distributed electric hydrogen coupling system for parks in this province was selected as an example for simulation analysis. The deviation rates for wind power generation, photovoltaic power generation, and demand response in the day-ahead, day-in, and real-time stages are set to 5%, 3%, and 1%, respectively. The unit scheduling costs for the first type of load demand response, the second type of load demand response, and the third type of load

demand response are 0.6, 0.85, and 1.00 yuan/kWh, respectively. According to the characteristics of each device, the response time for daily, intraday, and real-time scheduling is determined to be 30, 10, and 5 min, respectively. A distributed electric hydrogen coupling system was set up to connect to the external network at 10 kV and interact with the external network using the peak-to-valley electricity prices of general industrial and commercial industries from 1 to 10 kV in the province. At the same time, the specific purchase and sale electricity prices are shown in Table 1 (Tan et al., 2021; Han et al., 2022):

The operating parameters of various units are shown in Table 2 (Jiang et al., 2022):

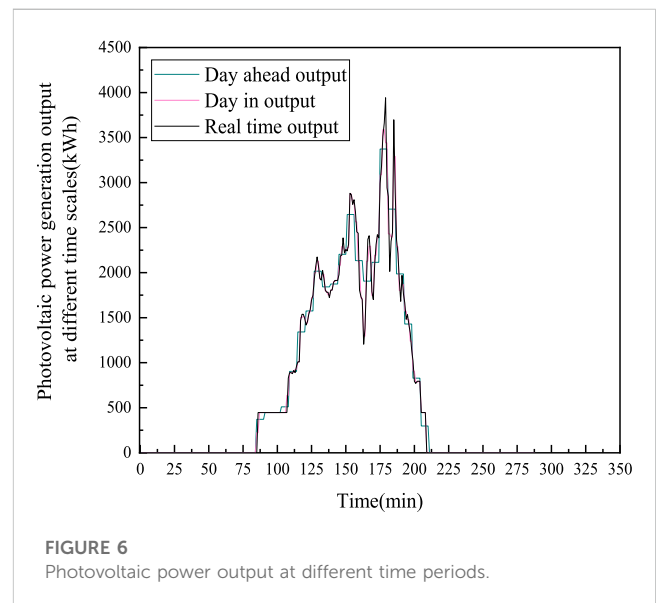
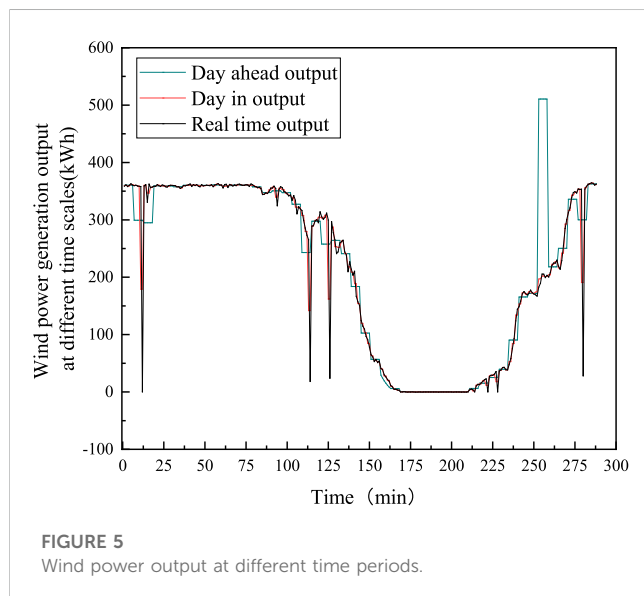
The day-ahead, day-in, and real-time predicted values for wind and photovoltaic power generation are shown in Figures 5, 6 (Tan et al., 2021):

TABLE 1 Electricity prices during peak and valley periods.

	Period of time	Electricity price (yuan/kWh)
Peak hour	19:00–21:00	1.1636
Rush hour	8:00–11:00, 13:00–19:00, and 21:00–22:00	0.8656
Valley period	11:00–13:00 and 22:00–8:00	0.3536

TABLE 2 Operating parameters of various units.

	Installed capacity	Upper power limit	Lower power limit	Upper climbing limit	Lower climbing limit
Wind turbines	400 KW	400 KW	0 KW	—	—
Photovoltaic panels	4 MW	4 MW	0 MW	—	—
Hydrogen fuel cell	240 KW	240 KW	48 KW	100%/min	—
Electric tank	400 KW	400 KW	80 KW	100%/min	—
Hydrogen storage tank	400 KG	—	—	—	—
Electric heat-transfer equipment	300 KW	300 KW	0 KW	52%/15 min	65%/15 min

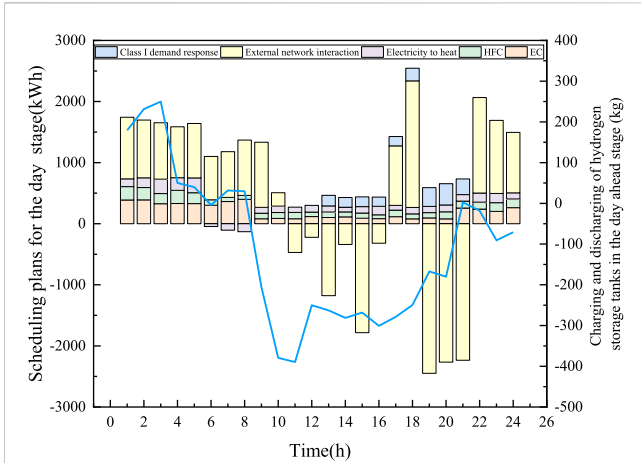


## 5.2 Example results

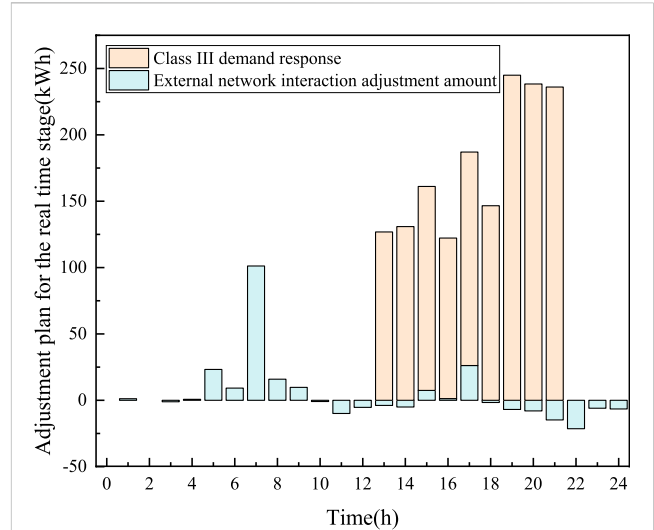
### 5.2.1 Scheduling optimization results for multiple timescales

Based on the predicted values of wind power generation, photovoltaic power generation, and various loads in real-time, in order to minimize the system operating cost, the scheduling optimization results at different timescales are obtained and analyzed. The optimization results of day-ahead, day-in, and real-time scheduling for each unit are shown in Figures 7–9, respectively. Due to the large amount of data under the 5-min scheduling time, the readability of the graph is poor. This paper selects one data at every 12 scheduling points to display day-ahead, day-in, and real-time stages in the graph.

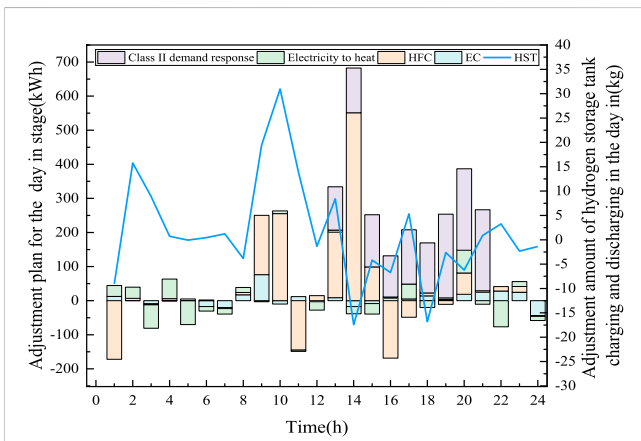
From Figures 7–9, it can be seen that the scheduling time for the first, second, and third types of demand response in the day-ahead, day-in, and real-time stages is approximately 19:00–22:00, overlapping with the peak load period. In order to maintain the balance between supply and demand in the recent stage, there are many challenges with the external network. Among them, the electricity purchase is carried out at 22:00–8:00 during the low-price period, and the low-price electricity is converted into hydrogen and stored in the hydrogen storage tank through the electrolytic cell equipment. During the peak power period, the hydrogen fuel cell consumes the hydrogen in the hydrogen storage tank to generate electricity. In the day-in stage, deviation adjustment is mainly carried out by adjusting the hydrogen storage tank and the second type of demand response. The adjustment amount of electric heat-



**FIGURE 7**  
Scheduling results in the day-ahead stage.



**FIGURE 9**  
Scheduling results in the real-time stage.



**FIGURE 8**  
Scheduling results in the day-in stage.

transfer equipment and electrolytic cells is relatively small, and only minor adjustments are made. In the real-time stage, compared to the day-ahead stage, the amount of interaction with the external network is significantly reduced. This is because the deviation in the real-time stage is reduced after adjustment in the day-in stage, and most of the deviation adjustment needs can be met through the third type of demand response.

### 5.2.2 Effectiveness analysis of uncertainty

In order to analyze and consider the effectiveness of system uncertainty, this paper sets up the following four scenarios for analysis:

Scenario 1: Set the wind and solar power output and load demand of the distributed electric hydrogen coupling system to be determined in three stages: day ahead, day in, and real time;

Scenario 2: Set the wind and solar output of the distributed electric hydrogen coupling system to be determined in three stages: day ahead, day in, and real time, taking into account the uncertainty of load demand in these three stages;

Scenario 3: Set the load demand of the distributed electric hydrogen coupling system to be determined in three stages: day ahead, day in, and real time, taking into account the uncertainty of wind and solar output in these three stages;

Scenario 4: Considering the wind power output and load demand of the distributed electric hydrogen coupling system simultaneously, uncertainty is determined in the three stages of day ahead, day in, and real time.

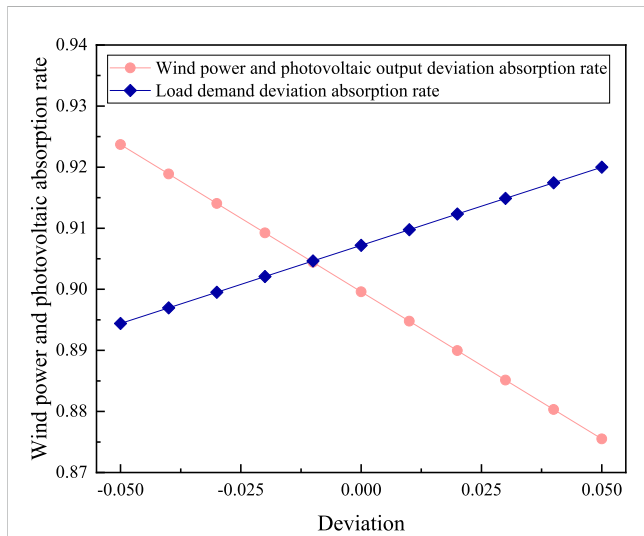
The scheduling costs of the distributed electric hydrogen coupling system in three stages under four scenarios are shown in Table 3.

From Table 3, it can be seen that among the four scenarios, scenario 1 under the deterministic scenario has the highest scheduling cost in the three stages of day ahead, day in, and real time, with a total scheduling cost of 40,289.79 yuan. Scenario 4, which simultaneously considers multiple uncertainties, has the lowest scheduling cost among the three stages, with a total scheduling cost of 35,231.9 yuan. Compared with Scenario 1, the total scheduling cost of Scenario 4 decreases by 12.55%. This is because uncertainty costs are not considered in deterministic scenarios. When there is a significant deviation between wind and solar power output and load demand, it will cause significant adjustments to the output of each unit in the day-in and real-time stages and even significantly increase the interaction cost with the external network, resulting in an increase in the overall adjustment cost. Although Scenario 2 considers the uncertainty of load, it does not consider the deviation of wind and solar output. On the one hand, when there is a significant deviation in wind and solar output, the accuracy of the unit output plan developed in the day-ahead stage is low. On the other hand, in the day-in and real-time stages, in addition to affecting the supply of electricity load, wind and solar power, as the supply end of electrolytic cells and electricity to heat transfer, will have an impact on the heat load and hydrogen load, increasing scheduling costs. Scenario 3 shows that the accuracy of load forecasting affects the scheduling of demand response. In the real-time stage, the third type of load demand invocation is mainly used. When the load deviation is large, the cost of daily adjustment increases. This indicates the necessity of considering the deviation between wind and solar output and load demand in distributed electric hydrogen coupling systems.

Furthermore, in order to explore the impact of wind and solar output deviation and load demand deviation on wind and solar consumption rate, taking the day-ahead stage as an example, the

**TABLE 3** Scheduling cost of the distributed electric hydrogen coupling system.

	Day-ahead scheduling cost (yuan)	Day-in adjustment cost (yuan)	Real-time adjustment cost (yuan)	Total scheduling cost (yuan)
Scenario 1	34846.44	3756.32	1687.03	40289.79
Scenario 2	32411.99	3206.53	1470.81	37089.33
Scenario 3	32849.23	3360.18	1449.24	37658.65
Scenario 4	31318.66	2801.39	1111.85	35231.9



**FIGURE 10** Wind power and photovoltaic absorption rates under different deviation rates.

wind and solar output deviation and load demand deviation rates were set to vary in the range (−5%, 5%). The wind and solar consumption rate under different deviation rates is shown in Figure 10.

As shown in Figure 10, when the negative deviation of wind and solar output increases in the opposite direction, the absorption rate of wind and solar energy increases. This is because when the load demand is constant and the reverse deviation rate of wind and solar energy increases, the system will fully absorb the wind and solar output, resulting in an increase in the absorption rate of wind and solar energy. When the load deviation rate increases positively, due to the increase in load demand, in order to ensure the balance of supply and demand and reduce other unit adjustments, the wind and solar output increases, resulting in an increase in the wind and solar consumption rate.

### 5.2.3 Effectiveness analysis of multi-timescale scheduling strategies

In order to evaluate the effectiveness of the multi-timescale optimization model proposed in this paper, effectiveness analysis that involves planning in the day-ahead stage and adjusting based on device priority in the day-in and real-time stages is demonstrated. On the one hand, it is compared with the key technologies proposed in Jin et al. (2019) in the two stages of “day-before-day-within-day”. On the other hand, it is compared with Liao et al. (2022), in which the model operates on a three-stage multi-timescale of “day-ahead-day-in-real-time” but does not consider the priority of device adjustment and the response characteristics of the device. The key technologies in Jin et al. (2019) and Liao et al. (2022) were applied to the distributed electro-hydrogen coupling system constructed in this paper. The cost and overall clean energy consumption rate of the system at different stages are shown in Table 4:

It can be seen from Table 4 that although there is no real-time stage cost in Jin et al. (2019), its day-ahead scheduling cost and day-in scheduling cost are far higher than Liao et al. (2022) and the proposed method. This is because in the current stage, Jin et al. (2019) did not make further adjustments and error correction in the real-time stage, which will lead to an increase in uncertainty and deviation costs. At the same time, the clean energy consumption rate of Jin et al. (2019) is lower than that of Liao et al. (2022) and the method proposed in this article. This is because from Figure 10, it can be seen that when the wind and solar deviation reaches 5% in the positive direction, the wind and solar consumption rate decreases, and there is no real-time adjustment, which cannot fully carry out new energy consumption, resulting in a decrease in the clean energy consumption rate. From this, it can be seen that it is necessary to conduct a three-stage scheduling of “day-ahead-day-in-real time.” Compared with the method proposed in this paper, the cost difference in the day-to-day stage is not significant, but the cost in the day-in stage and the real-time stage is higher than that of the method proposed in this paper. This is because Liao et al. (2022) did not

**TABLE 4** Cost and overall clean energy consumption rate of the system at different stages.

	Day-ahead scheduling cost (yuan)	Day-in adjustment cost (yuan)	Real-time adjustment cost (yuan)	Total scheduling cost (yuan)	Clean energy consumption rate (yuan) (%)
Jin et al. (2019)	35,079.52	6,336.05	—	41,415.57	76.46
Liao et al. (2022)	33,150.80	4,420.43	2,518.58	40,089.81	84.13
This paper	32,849.23	3,360.18	1,449.24	37,658.65	89.96

TABLE 5 Evaluation indicators for scheduling timescale optimization.

	$\omega_{sh}$			$N^{tz}$	$\psi_{tz}$
	Electricity (%)	Heat (%)	Hydrogen (%)		
Yuan et al. (2019)	4.26	7.84	2.97	860	54.84%
Bao et al. (2016)	3.35	6.89	7.75	748	46.75%
This paper	2.1	2.01	4.26	672	45.85%

consider the level of equipment adjustment and response characteristics, which cannot achieve efficient coordination and optimization among various devices and resource allocation, resulting in an increase in cost.

### 5.2.4 Effectiveness analysis of scheduling timescale optimization

In order to analyze the effectiveness of scheduling timescale optimization proposed in this paper, the evaluation indicators in Li et al. (2023) were compared with those in Yuan et al. (2019) and Bao et al. (2016). The comparison indicators are the supply and demand imbalance rate  $\omega_{sh}$ , the number of real-time adjustments within the day  $N^{tz}$ , and the proportion of adjustments  $\psi_{tz}$ , as shown in Eqs 24–26, respectively:

$$\omega_{sh} = \frac{\sum_{s=1}^4 \sum_{y=1}^{15} \frac{|P_{sup, sy}^{total} - L_{dem, sy}^{total}|}{L_{dem, sy}^{total}}}{n_{dem}}, \quad (24)$$

$$N^{tz} = \sum n_i^{tz}, \quad (25)$$

$$\psi_{tz} = \frac{\sum n_i^{tz}}{n_{total}^{sb}}, \quad (26)$$

where  $P_{sup, sy}^{total}$  and  $L_{dem, sy}^{total}$  are the total aggregate supply and demand of energy, respectively;  $n_{dem}$  is the total number of load data;  $n_i^{tz}$  is the number of adjustments made by device  $i$  during the day-in and real-time phases,  $i \in \{dj, hf, EH, EHS\}$ ; and  $n_{total}^{sb}$  represents the total number of devices.

The supply and demand imbalance rate  $a$ , daily real-time adjustment frequency  $b$ , and adjustment proportion  $c$  of Yuan et al. (2019), Bao et al. (2016), and this paper are shown in Table 5.

From Table 5, it can be seen that compared with Bao et al. (2016), using the method proposed in this paper for scheduling time optimization can reduce the supply–demand imbalance rate and ensure the stability of energy supply in the distributed electric hydrogen coupling system. On the other hand, compared with Jin et al. (2019) and Yuan et al. (2019), the method proposed in this paper has lower frequency and proportion of adjustments in these two indicators. This is because this article considers the response characteristics of heterogeneous energy sources such as electricity and heat loads and coupled equipment, which can coordinate the slow response time of heat loads and coupled equipment, as well as the fast response characteristics of wind, electricity loads, and hydrogen storage tanks. Therefore, the scheduling duration optimization method proposed in this article can simultaneously balance the dual optimization strategy of adjusting costs and energy supply stability.

## 6 Conclusion

This paper conducts a study on the optimization of multi-timescale operation of distributed electro-hydrogen coupling systems considering multiple uncertainties. Through case analysis, the following conclusions are drawn:

- (1) It is necessary to consider the deviation between wind and solar output and load demand in a distributed electric hydrogen coupling system, and it can reduce the total scheduling cost by 12.55% compared to deterministic scenarios.
- (2) The three-stage scheduling optimization strategy proposed in this article, which considers the level of equipment adjustment and response characteristics, can achieve efficient coordination and optimization among various devices, optimize resource allocation, and improve the consumption rate of clean energy.
- (3) The scheduling duration optimization method proposed in this article is a dual optimization strategy that simultaneously considers adjustment costs and energy supply stability.

## Data availability statement

The original contributions presented in the study are included in the article/Supplementary Material; further inquiries can be directed to the corresponding author.

## Author contributions

SMA: visualization and writing—review and editing; SME: validation; LY: supervision and project administration. All authors contributed to the article and approved the submitted version.

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## Conflict of interest

Authors SMA and SME were employed by Guangdong Power Grid Co., Ltd. LY was employed by Dongguan Power Supply Bureau of Guangdong Power Grid Co., Ltd.



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## Nomenclature

Parameters	
$\eta_{wind,t}$	output coefficient of the wind power plant at time $t$
$m_{pv}$	area of the photovoltaic panel
$\lambda_{pv}$	efficiency of the photovoltaic panel in absorbing light intensity
$\lambda_{loss}$	loss coefficient of the photovoltaic panel
$\lambda_{el,t}^I, \lambda_{el,t}^U$	current efficiency and voltage efficiency of the electrolytic cell
$U_{el}^{rev}, U_{el}^{ohm}, U_{el}^{h2}, U_{el}^{o2}$	reversible voltage, resistance voltage drop, hydrogen overpotential, and oxygen overpotential, respectively
$R_{el}$	resistance of the electrolyte
$\theta_1, n_1, j_1$	charge transfer coefficient, electron transfer number, and current density of the cathode, respectively
$c_1, c_2$	Fan's coefficient
$V_{EHS,t}$	volume of the hydrogen storage tank
$M_H$	relative molecular weight of hydrogen gas
$m_{EHS,t}^{in}$	hydrogen mass of the hydrogen storage tank at time $t$
$m_{hf,t}$	hydrogen consumed by the hydrogen fuel cell
$H_{hf,t}^{loss}$	heat energy lost by the hydrogen fuel cell
$V_{hf}$	operating voltage of the hydrogen fuel cell
$\lambda_{EH,t}$	conversion efficiency of the electric heat-transfer equipment
$P_{wind,t}^{D,min}, P_{wind,t}^{D,max}$	upper and lower limits of wind power generation, respectively
$G_{P_{pv,t}}$	uncertainty set of photovoltaic power generation
$\eta_{pv}$	Robustness factor for the uncertainty set of photovoltaic power generation
$\bar{L}_{ele,t}, \bar{L}_{heat,t}, \bar{L}_{hy,t}$	expected electrical load, thermal load, and hydrogen load at time $t$ , respectively
$m_{EHS,t}^{rq-in}, m_{EHS,t}^{rq-out}$	hydrogen storage and release capacity of the hydrogen storage tank at time $t$ ; kg, respectively
$p_{PDR}^1$	first type of demand response unit scheduling cost; yuan/kWh
$p_i^{\min}, p_i^{\max}$	minimum and maximum output of unit $i$ ; kWh, respectively
$H_{EH}^{\min}, H_{EH}^{\max}$	minimum and maximum output of the electric heat-transfer equipment, respectively
$m_{EHS}^{\min}, m_{EHS}^{\max}$	minimum and maximum hydrogen storage capacity of the hydrogen storage tank, respectively
$\Delta m_{dj}^{\min}, \Delta m_{dj}^{\max}$	minimum and maximum values for climbing the electrolytic cell slope, respectively
$p_{PDR}^2$	scheduling unit scheduling cost for the second type of demand response; yuan/kWh
$u_{EHS}^{rn-tz}$	unit-adjusted cost of the hydrogen storage tank; yuan/kg
$u_{hf}^{ss-tz}$	unit adjustment cost of the hydrogen fuel cell in the real-time phase; yuan/kWh
$P_{wind}^e$	rated power of the wind power plant; kWh
$f_{pv,t}$	light intensity at time $t$
$\lambda_{tran}$	solar-cell efficiency
$m_{dj,t}^{out}, \lambda_{el,t}$	quality and efficiency of hydrogen gas produced by the electrolytic cell
$I_{el}^t$	operating current of the electrolytic cell
$TP_j$	temperature, pressure, and current density
$EY$	universal gas and Faraday constant

$\vartheta_2 n_2 j_2$	charge transfer coefficient, electron transfer number, and current density of the anode
$n_{EHS,t}$	amount of hydrogen in the hydrogen storage tank
$T_H$	temperature of hydrogen gas
$m_{EHS,t+1}$	hydrogen mass of the hydrogen storage tank at time $t+1$
$m_{EHS,t}^{out}$	hydrogen-release amount of the hydrogen storage tank at time $t$
$P_{hf,t} H_{hf,t}^{ct}$	electric energy and thermal energy generated by the hydrogen fuel cell
$\lambda_{hf,t}$	Electrical efficiency of the hydrogen fuel cell
$\Delta H_{h_2}$	enthalpy value of hydrogen gas
$G_{P_{wind,t}}$	uncertainty set of wind power generation
$\eta_{wind}$	robustness factor for the uncertainty set of wind power generation
$P_{pv,t}^{D,\min} P_{pv,t}^{D,\max}$	upper and lower limits of photovoltaic power generation, respectively
$P_{buy} P_{sale}$	unit electricity purchase cost and unit electricity sales cost when the distributed electric hydrogen coupling system interacts with the external network; yuan/kWh, respectively
$\varepsilon_{ele} \varepsilon_{heat} \varepsilon_{hy}$	expected deviation rate between electrical load, thermal load, and hydrogen load
$P_{wind} P_{pv} P_{dj} P_{hf} P_{EHS} P_{EH}$	Unit operating cost of the wind turbine generator set, photovoltaic generator set, electrolytic cell, hydrogen fuel cell, hydrogen storage tank, and electric heat-transfer equipment; yuan/kWh, respectively
$v_{pun}$	unit uncertainty cost; yuan
$\Delta P_i^{\min} \Delta P_i^{\max}$	minimum and maximum values for unit $i$ to climb the slope, respectively
$\Delta H_{EH}^{\min} \Delta H_{EH}^{\max}$	minimum and maximum values for the climbing of the electric heat-transfer equipment, respectively
$m_{dj}^{\min} m_{dj}^{\max}$	minimum and maximum output of the electrolytic cell, respectively
$L_{PDR,t}^{\min,1} L_{PDR,t}^{\max,1}$	minimum and maximum scheduling amount for the first type of demand response, respectively
$u_{dj}^{n-tz} u_{hf}^{n-tz} u_{EH}^{n-tz}$	Unit adjustment cost of electrolytic cell, hydrogen fuel cell, and electric-to-heat equipment in the day stage; yuan/kWh, respectively
$\rho_{PDR}^3$	Scheduling unit scheduling cost for the third type of demand response; yuan/kWh