



# Mudstones as Landfill Liner Material for Heavy Metal Removal: Equilibrium and Dynamic Sorption Study

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**Abstract** Clay materials used as low-permeability barriers at landfill sites can also chemically attenuate inorganic contaminants (heavy metals) in leachate. In this study, Cu(II) removal capacity from aqueous media of a raw calcareous mudstone, used as a liner material, was evaluated through both batch and column tests. Batch experiments were conducted varying contact time, pH, and Cu(II) concentration. In order to simulate waste leachates composition, the effect of the presence of some organic compounds on Cu(II) uptake was also evaluated. Column tests of

compacted calcareous mudstone-sand mixtures were performed to evaluate sorption in dynamic systems. The studied calcareous mudstone exhibited higher removal capacity in a wider pH range than a commercial Na-bentonite, which is a widely used heavy metal sorbent and clay liner. It was evidenced that calcite, an important component of the calcareous mudstone and found as very small and highly porous calcareous nanofossils, contributed to its sorption properties playing a significant role in the Cu(II) removal. The presence of an anionic surfactant or phenol slightly affected the removal of Cu(II). In the clay fraction (< 2 µm), Cu(II) sorption was favored by the presence of humic acids, which add new adsorption sites

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for this metal. The extremely high retardation factor obtained for the raw calcareous mudstone is in good agreement with the high adsorption capacity experimentally proved in batch tests and demonstrated a great ability of this material to retain heavy metal mass during the transport in solution within porous media.

**Keywords** Clay liners · Heavy metal · Calcite · Adsorption · Precipitation · Leachate

## 1 Introduction

One of the main concerns in urban landfills is the possible migration of leachate with the consequent soil and groundwater contamination. Leachates represent complex mixtures of substances including dissolved organic matter, inorganic matter (ammonia–nitrogen, nitrate–nitrogen, total phosphorus), inorganic macro-components, heavy metals, and a wide range of xenobiotic organic compounds (Kjeldsen et al., 2002; Ye et al., 2019). Many of these substances are hazardous and toxic to human health and the environment (Vaverková et al., 2019). Heavy metals such as Cu(II), Zn(II), Cd(II), and Ni(II) are considered harmful for human health when exceed the tolerance levels and are frequently founded in large amounts in different kinds of waste and landfill leachates (Cuevas et al., 2008; Kylefors, 2003; Lo et al., 2009; Long et al., 2011; Suna Erses et al., 2005). Therefore, migration of these compounds must be avoided and leachate should not migrate outside landfill cells to reduce their impact on the ecosystems.

Leachate migration is commonly controlled by a multiple barrier system that includes geomembranes and compacted clay liners with a low hydraulic conductivity and a high adsorption capacity (Bouazza & Van Impe, 1998; Rowe, 2005). Bentonites have been used for many years as a component of clay liners due to their suitable physical and chemical properties to isolate flow and adsorb heavy metals (Atkovska et al., 2016; Ayari et al., 2005; Koch, 2002; Li et al., 2015; Mishra et al., 2011; Musso et al., 2016; Nath, 2020; Scalia et al., 2018). In this application, they are generally utilized in combination with natural soils or sand and synthetic materials (e.g., compacted clay liners (CCL) or geosynthetic clay liners (GCL)) (Daniel, 1993).

Heavy metal sorption from aqueous solutions through clay minerals is highly influenced by pH and ionic strength (Chen et al., 2011; Francisca & Glatstein, 2020; Mnasri-Ghnmia & Frini-Srasraa, 2019). In a landfill leachate, these parameters change with time. During the initial phase of a landfill, leachate pH is acid and later, in a methanogenic stage, the pH increases giving a range of pH between 4.5 and 9.0 depending on the landfill stabilization (Christensen et al., 2001). Despite studies about clay minerals behavior as adsorbents are usually referred to the adsorption of single compounds (organic or inorganic), wastewaters or leachates from waste deposits, usually contain both inorganic and organic compounds which compete for the adsorption sites (Ayala et al., 2008; Kylefors, 2003). The type and concentration of organic compounds present in a landfill leachate depend not only on the kind of waste but also on the landfill age (Paxéus, 2000; Rigobello et al., 2015). Humic substances, surfactants, and phenolic compounds are some of the organic compounds that can be found in landfill leachates (Christensen et al., 2001; Reitzel & Ledin, 2002; Sakai et al., 2000). In general, organic compounds affect the sites adsorption reactivity of clay minerals (Wu et al., 2015; Zhang et al., 2015). Moreover, humic substances play an important role retaining heavy metals due to its hydrophilic nature and ionizable oxygen groups (Covelo et al., 2007).

Most of the studies looking at heavy metal sorption by clay minerals have been conducted in batch setups and fewer studies deal with adsorption in dynamic systems. In the design of containment barriers, an understanding of the attenuation characteristics of clay liner components would improve barrier performance (Thornton et al., 2001). Column experiments can be used as an alternative to investigate the sorption and transport of metals and are considered to reflect field conditions of landfill clay liners allowing the evaluation of removal processes for large-scale applications (Contreras et al., 2017; Refaey et al., 2017).

Mudstones represent the major constituents of sedimentary basins worldwide. They are low-permeability sedimentary rocks with a high sorption capacity; consequently, they are important natural barriers that restrict leakage from waste disposal sites (Lin & Cheng, 2006). Numerous outcrops of Cretaceous–Tertiary calcareous mudstones are found in North

Patagonia Argentina. These mudstones are mainly composed of smectitic clay minerals and have suitable hydraulic properties to be used as clay liners when are compacted with sand (Musso et al., 2013). In addition to their known quality as physical barriers, some studies in equilibrium conditions performed on the clay fraction ( $< 2 \mu\text{m}$ ) have demonstrated that these mudstones have a high heavy metal adsorption capacity from monometal solutions (Musso et al., 2014, 2017). Although this efficiency related to metal removal from aqueous solutions was previously described, there is no information on the sorption capacity of the raw material (clay minerals + non-clay minerals), which is the natural extraction condition in the quarry and the way this material is used in practical applications (e.g., landfill liners or surface impoundments). On the other hand, to the best of our knowledge, there are no adsorption studies performed on these mudstones from solutions containing organic and inorganic components as is the case of real leachates.

This paper focuses particularly on Cu(II) metal as model contaminant since it is one of greatest concern for regulators in terms of groundwater contamination through landfill leachates (Kaoser et al., 2005). Thus, the aim of the present study was to investigate the capacity of raw calcareous mudstones in the removal of Cu(II) from water through equilibrium and dynamic adsorption tests and to assess the effect of pH and organic compounds on the Cu(II) uptake.

## 2 Materials and Methods

### 2.1 Materials and Chemicals

A calcareous mudstone, named NTOL, was used to evaluate its potential as a sorbent material for Cu(II) uptake. This material belongs to Jagüel Formation of the Neuquén basin, North Patagonia Argentina. The mudstone meets the technical requirements outlined in the European, Japanese, and American legislations for use as clay liners (Chai & Miura, 2002), having hydraulic conductivities lower than  $1 \times 10^{-9} \text{ ms}^{-1}$  permeated with water and with real leachate in mixtures with sand (Musso et al., 2017). For comparison purposes, a commercially available bentonite, named CATAE, was used as a reference material performing as well, all the tests on this clay. The mudstone and

the bentonite have the consistency of hard rock and were crushed and then milled resulting in powdered samples with a size of about  $80 \mu\text{m}$ . Physicochemical and mineralogical properties of the samples were previously published (Table S1, in the supporting information).

A high resolution LEO 1530 (Zeiss) scanning electron microscope (SEM) was used to observe the morphology of the mineralogical constituents of the calcareous mudstone.

In order to complete the characterization of the sorbents, thermal analysis, both, thermogravimetric (TGA) and differential thermal analyses (DTA) were carried out by a Simultaneous Thermal Analyzer (Netzsch STA 409/c). The non-isothermal analysis was conducted in the temperature range of  $20\text{--}1100 \text{ }^\circ\text{C}$  at  $10 \text{ }^\circ\text{C}/\text{min}$  heating rate and in circulating air atmosphere.

For the column experiments, the clays were mixed with a commercial fluvial sand classified as poorly graded ("SP" according to the Unified Soil Classification System), to simulate typical isolation materials used in liners.

Analytical grade  $\text{Cu}(\text{NO}_3)_2 \cdot 3\text{H}_2\text{O}$  salt used as Cu(II) source was purchased from Sigma-Aldrich Co. and metal quantification was performed by atomic absorption spectroscopy (AAS) (Analyst 200, Perkin-Elmer). NaOH and HCl solutions were used for pH adjustment, and 0.08 M of NaCl solution was prepared for ionic strength control. Leonardite humic acid (LHA) was purchased from International Humic Substances Society. Commercial LAS (sodium salt of dodecylbenzene sulfonate, 80%) and phenol (98%) from Sigma Chemical Company Ltd. were used as received.

### 2.2 Methods

#### 2.2.1 Batch Sorption Tests

Adsorption kinetics was initially done to evaluate the time needed to achieve equilibrium of Cu(II) adsorption by the raw calcareous mudstone and bentonite. A total of 0.635 g of sorbent was added to 500 mL of  $3 \text{ mg L}^{-1}$  initial Cu(II) solution at  $\text{pH}=5.5$ . The flask was then placed on a shaker (200 rpm) under constant agitation at  $25^\circ \pm 1 \text{ }^\circ\text{C}$ . At regular intervals, 10 mL of solution was withdrawn, filtered through a  $0.45 \mu\text{m}$  syringe acetate filters

(Scharlab) and the concentration of the remaining Cu(II) in solution ( $C$ ) was measured. The amount of Cu(II) adsorbed at a time  $t$  was calculated by the difference between the initial and the final Cu(II) concentration (Eq. 1) as follows:

$$q_e = \frac{(C_i - C_e) * V}{W} \quad (1)$$

where  $q_e$  is the equilibrium concentration of Cu(II) in solid phase ( $\text{mg g}^{-1}$ );  $C_i$  and  $C_e$  are the initial and equilibrium concentrations ( $\text{mg L}^{-1}$ ) of Cu(II) in solution, respectively; and  $V$  and  $W$  represent the volume of the solution (L) and mass of the sorbent (g), respectively.

Monometal adsorption isotherms were obtained by mixing 0.031 g of raw clay sample with 25 mL of metal solutions containing various concentrations of Cu(II) (3–220  $\text{mg L}^{-1}$ ). The lower concentrations of these solutions are similar to the average Cu(II) concentrations determined in an Argentinean urban waste leachate (Francisca & Glatstein, 2010). The solutions were prepared using NaCl (0.08 M) as electrolyte, and the pH of the metal solution was adjusted to 5.5 using an Altronix EZDO-PC pH meter. The pH and ionic strength were selected to simulate a leachate in the acetogenic stage. The mixtures were shaken in a rotative shaker for 6 h at 25 °C. Then the specimens were centrifuged at 3600 rpm for 20 min and the supernatant was filtered through 0.45  $\mu\text{m}$  syringe acetate filters (Scharlab) and stored in polypropylene tubes. The amount of metal adsorbed in the clay was calculated by mass balance from the initial concentration  $C_i$ , and the final (equilibrium) concentration  $C_e$ , in the supernatant following Eq. 1. All batch tests described in this section were performed in duplicate in order to verify the reproducibility of results. Experimental results were analyzed using Langmuir and Freundlich isotherm models, Eqs. (2) and (3), respectively:

$$q_e = \frac{C_s \cdot K_L \cdot C_e}{1 + K_L C_e} \quad (2)$$

$$q_e = K_F \cdot C_e^{1/n} \quad (3)$$

where  $C_s$  is the maximum adsorption capacity ( $\text{mg g}^{-1}$ ),  $K_L$  is the adsorption coefficient of the

Langmuir model ( $\text{L mg}^{-1}$ ), and  $K_F$  and  $n$  are Freundlich constants which correspond to adsorption capacity and adsorption intensity, respectively.

In the study of pH effect on Cu(II) removal, the same procedure to obtain adsorption isotherms was carried out. For these experiments, Cu(II) concentration was 2.5  $\text{mg/L}$  in order to assure the exclusive presence of aqueous Cu(II) species in all the analyzed pH range. pH range studied was 3–9 to simulate the typical pH-range found in the leachate during the aging of landfills. In this case, ionic strength condition was maintained constant at 0.08 M. In order to evaluate the dissolution of calcite, a portion of the supernatant obtained from the pH effect experiment after the adsorption of Cu(II) was separated for calcium analysis by AAS.

Different concentrations of HA (1–10–50  $\text{mg/L}$ ), phenol (1–25–50  $\text{mg/L}$ ), and anionic surfactant (LAS) (1–25–50  $\text{mg/L}$ ) were tested with the aim of describing their effect on the sorption of Cu(II) on clay materials. HA effect was also evaluated on clay fraction ( $<2 \mu\text{m}$ ). The supernatant of clay-HA (50  $\text{mg/L}$ )-Cu(II) complexes after they have reached equilibrium was analyzed by UV-spectroscopy to quantify the percentage of HA retained by the clay.

### 2.2.2 Column Sorption Test

Continuous flow columns tests were used to evaluate Cu(II) uptake in dynamic systems on calcareous mudstone-sand mixtures and bentonite-sand mixtures. The composition of the columns was 25% of NTOL and 12% of CATAE using sand as a granular material. These percentages were selected considering hydraulic requirements stipulated by international regulations to be used as isolating barriers (Musso et al., 2017). The samples were prepared by mixing sand, powder mudstone/bentonite, and tap water and cured in plastic bags for 24 h. The water content of the mixtures was 2% wet of the optimum water content (i.e., 12.5%) obtained in previous Proctor Compaction Tests (ASTM D698-07e1 2007). Subsequently, the samples were compacted in rigid wall columns and the procedure for hydraulic conductivity measurements by the falling head method was followed (ASTM D5856-95 2007). The column test set up is shown schematically in Fig. S1, in the supporting information. The samples were permeated initially with deionized water and subsequently, with

the Cu(II) solution containing 10 mg L<sup>-1</sup> of Cu(II). pH and ionic strength of the solution were adjusted to 5.5 and 0.08 M respectively.

The metal concentration, *C*, of the effluent collected from the bottom of the column was measured over time plotting the results as solute breakthrough curves (relative concentration (*C/C*<sub>0</sub>) versus pore volumes (PV)). The value of number of pore volume effluent (PVE) necessary to reach a ratio of *C/C*<sub>0</sub>=0.5 is used to calculate retardation and adsorption coefficients (Sharma & Reddy, 2004). All measurements were conducted in triplicate.

**Numerical Modeling of Mass Transport** The expected behavior of the metal transport through the soil columns is controlled by the well-known advection and hydrodynamic dispersion with sorption equation (Sharma & Reddy, 2004):

$$D_L^* \frac{\partial^2 C}{\partial x^2} - v_e \frac{\partial C}{\partial x} \pm \frac{r}{n_e} = \frac{\partial C}{\partial t} \quad (4)$$

where *C* (kg/m<sup>3</sup>) is the contaminant concentration, *D*<sub>L</sub><sup>\*</sup> (m<sup>2</sup>/s) is the longitudinal hydrodynamic dispersion coefficient, *n*<sub>e</sub> is porosity, *v*<sub>e</sub> (m/s) is the seepage velocity, *r* = -(*B*<sub>d</sub>/θ) · (∂*C*<sup>\*</sup>/∂*t*) (kg/m<sup>3</sup>/s) is the rate of mass consumption due to reaction inside the porous media, *B*<sub>d</sub> (kg/m<sup>3</sup>) is bulk density of porous media, θ is the volumetric water content (=porosity for saturated media), and *C*<sup>\*</sup> is the adsorbed mass on soil particles per unit weight of solids. The amount of either Cu(II) or any other metal adsorbed is related to the initial concentration by means of Eqs. (2) and (3).

Sorption columns can be simulated as 1D problem and therefore the analytical solution provided by Ogata and Banks (1961) can be used to predict the evolution of metal concentration over the space and time:

$$C_{(x,t)} = \frac{C_0}{2} \operatorname{erfc} \left[ \frac{R \cdot x - v_e \cdot t}{2 \sqrt{D_L^* \cdot t \cdot R}} \right] \quad (5)$$

where *R* is the retardation factor estimated in this work from the calibrated Langmuir isotherms according to Eq. 6 (Sharma & Reddy, 2004):

$$R = 1 + \frac{B_d}{\theta} \left[ \frac{K_L \cdot C_s}{(1 + K_L \cdot C_e)^2} \right] \quad (6)$$

### 3 Results and discussion

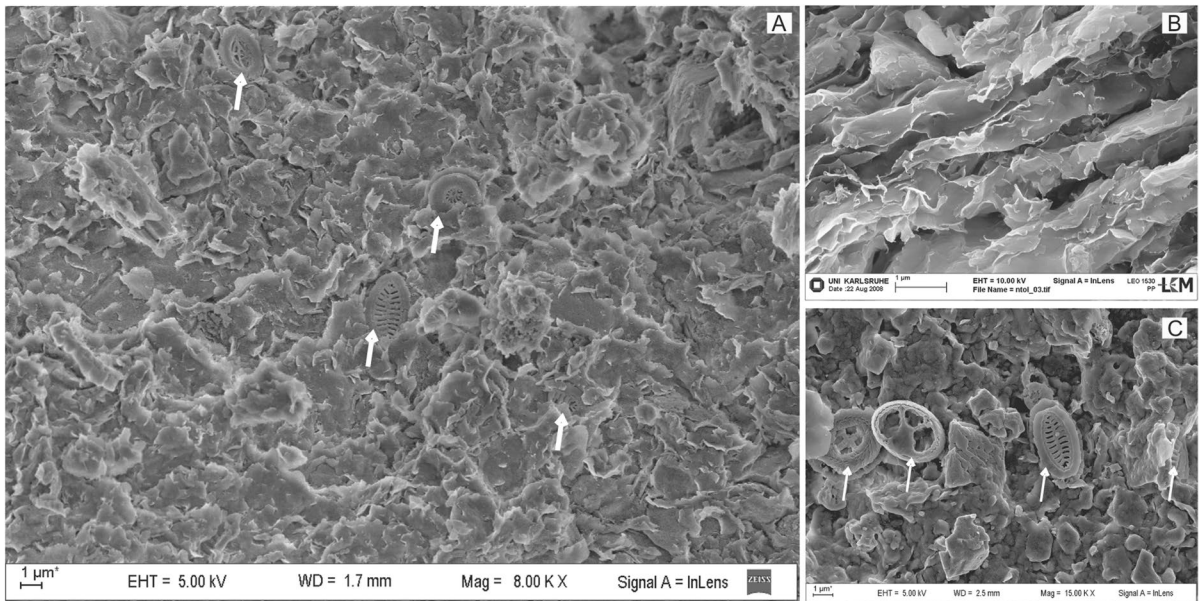
#### 3.1 Characterization of the Sorbents

The mineralogy of the mudstone is dominated by a R0 illite/smectite mixed layer (80% Sm), with a slightly crenulated to flaky morphology and biogenic calcite (calcareous nannofossils) (10%) (Fig. 1) (Table S1 in the supporting information). Calcareous nannofossils are mainly constituted by coccoliths which consists of minuscule CaCO<sub>3</sub> structures produced by unicellular phytoplankton (Müller 2019). The size of the coccoliths is between 2 and 3 μm and they are highly porous (Fig. 1A and C).

Thermal analyses of the samples are presented in Fig. S2, in the supporting information. The curves show that the bentonite had a higher percentage of mass loss than the calcareous mudstone in the studied temperature range (18% vs 13%, respectively). In both cases, the main losses are due to 8–10% removal of adsorbed and interlayer water (0–300 °C), 2–4% removal of OH groups (dehydroxylation) (560–690 °C), and 3–4% corresponding to a S-shaped endo-exotherm at 850–950 °C which indicates the formation of new phases (Fajnor and Kesenák, 1996). Differences in dehydroxylation temperatures between the analyzed materials are related to the existence of OH groups in various local environments in the case of the interstratified 2:1 clay mineral in NTOL. Also, in calcareous mudstone NTOL, an additional endothermic peak is observed at 811 °C related to decomposition of calcite into CaO and release of CO<sub>2</sub> (Shahraki et al., 2011) confirming also the presence of this mineral phase in the mudstone.

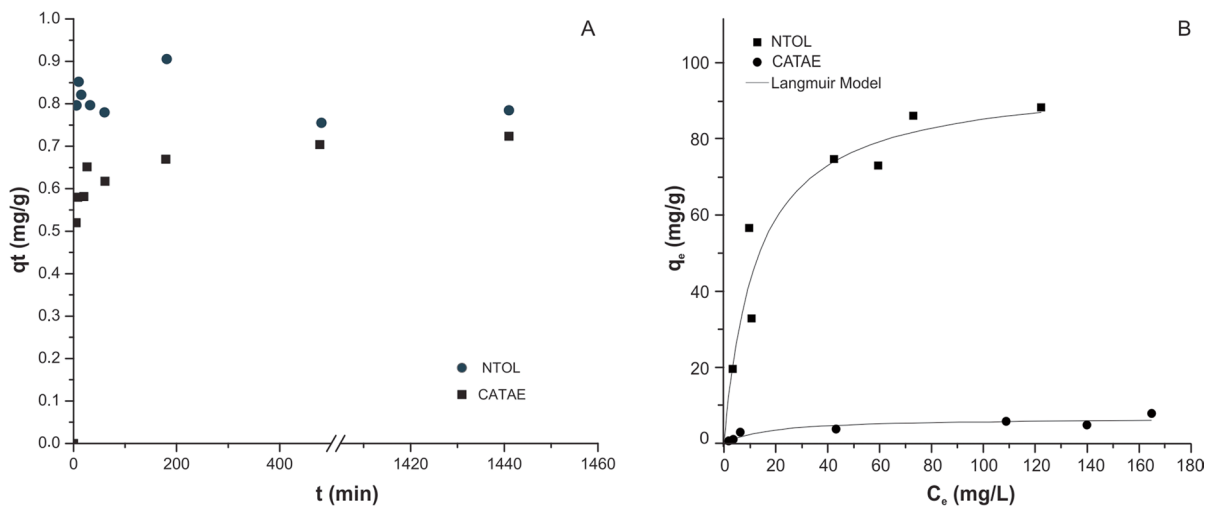
#### 3.2 Effect of Contact Time on Cu(II) Sorption

Figure 2A shows the amount of Cu(II) removed with respect to contact time. For the bentonite CATAE, it is observed that the rate of removal from solution was initially fast in the first 50 min and then diminished gradually until an equilibrium time beyond which there was no significant increase in the removal rate (at ~ 1400 min). On the other hand, in NTOL mudstone, the reaction was almost instantaneously achieving equilibrium removal before 5 min of contact and revealing an ultrafast removal rate compared with the bentonite. This is in agreement with other sorption studies performed on



**Fig. 1** **A** SEM image of NTOL calcareous mudstone showing oriented bioclasts (calcareous nanofossils) scattered in a laminated clay groundmass (white arrows). **B** Illite/smectite-mixed

layer particles showing crenulated morphology and laminar microfabric. **C** Detail of the high porosity of coccoliths included in clay (white arrows)



**Fig. 2** **A** Effect of contact time on Cu(II) sorption. Initial metal concentration 3 mg/L, clay dosage 0.635 g/500 mL, pH 5.5,  $T=25$  °C. **B** Sorption isotherms of Cu(II) of the calcareous mudstone NTOL and the bentonite CATAE

calcareous materials which also reported very fast kinetics (Perez-Sirvent et al. 2019). This information indicates that all adsorption data obtained after these times can be considered obtained under equilibrium conditions.

### 3.3 Effect of Metal Concentration on Cu(II) Sorption

Sorption isotherms of Cu(II) of the calcareous mudstone and the bentonite are shown in Fig. 2B. In both materials, sorption isotherms follow L-shaped type

similar to that described by Sposito (1984) indicating a high affinity between sorbent and solute. However, at low initial concentrations, NTOL isotherms have a much higher slope than CATAE isotherms revealing a higher affinity for NTOL which decreases as Cu(II) concentration increases.

The Langmuir and Freundlich isotherms were used to model the experimental data (Table 1). The obtained Freundlich parameters showed that the adsorption intensities ( $n_f$ ) were higher than 1 (1/n closer to 0) showing that the adsorption process is more likely to be heterogeneous (Fierro et al., 2008). The Freundlich constants ( $K_F$ ) show the interaction between metal ions and adsorbents, and the higher this value, the better adsorption will proceed (Kakaei et al., 2020). In this regard, NTOL sample had higher  $K_F$  than the bentonite CATAE.

The  $C_s$  value of NTOL calcareous mudstone for adsorbing Cu(II) was 15 times higher than the bentonite CATAE (Table 1) and also significantly higher than other calcareous materials (Table 2). On the other hand, the  $C_s$  of the bentonite CATAE for Cu(II) was close to those values reported in literature for other Na-bentonites (<10 mg/g) (Abollino et al., 2003; Andini et al., 2006; García-Sánchez et al., 1999; Ling et al., 2007).

Even though the calcareous mudstone has a higher adsorption capacity, cation exchange capacity value for NTOL sample is almost the half than the bentonite CATAE (Table S1 in the supporting information). This indicates that the intrinsic ion exchange capacity of this sample is not high enough to remove

large amounts of Cu(II) via ion-exchange mechanism. Therefore, these results would reflect the influence of the mineralogical differences between the calcareous mudstone and the bentonite in sorption processes.

In NTOL calcareous mudstone, three mineral components could be involved in Cu(II) removal processes from the solution: (1) the smectitic clay component of the I/S-mixed layer; (2) illite, and (3) calcite. Mechanisms of Cu(II) sorption on the smectitic clay component of the I/S-mixed layer would be cationic exchange reactions with  $Ca^{2+}$  and  $H^+$  ions located in the basal surfaces and at the edges of clay particles, respectively (Abollino et al., 2003; Kaya & Ören, 2005; Musso et al., 2019; Vhahangwele & Mugeru, 2015; Zhang et al., 2011). In the case of illite, previous results have shown that the percentage of this clay mineral becomes an important factor in metal adsorption at pH higher than 6 where complexation reactions on the edge sites predominate (Alvarez-Puebla et al., 2005; Gu & Evans, 2007; Missana et al., 2008; Wu et al., 2011).

Heavy metals can be sorbed on the surface of calcite which has been described as a significant metal-scavenging process in water and soil environments as well as in waste systems (García-Sánchez & Alvarez-Ayuso, 2002). In NTOL mudstone, calcite is in the form of very small and highly porous bioclasts (calcareous nanofossils) (Fig. 1) which would contribute with a higher BET specific surface (Table S1 in the supporting information) and therefore with sorption processes. Most common sorption processes onto calcite surface include outer-sphere or inner-sphere

**Table 1** Isotherms coefficients according to Freundlich and Langmuir

|                    | Freundlich  |       |       | Langmuir     |              |       |
|--------------------|-------------|-------|-------|--------------|--------------|-------|
|                    | $K_F$ (L/g) | $n_f$ | $R^2$ | $K_L$ (L/mg) | $C_s$ (mg/g) | $R^2$ |
| NTOL total sample  | 11.65       | 2.26  | 0.84  | 0.05         | 103.24       | 0.93  |
| CATAE total sample | 0.80        | 2.42  | 0.88  | 0.05         | 6.75         | 0.85  |

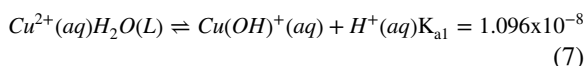
**Table 2** Comparison of Langmuir maximum adsorption capacities ( $C_s$ ) of other natural calcareous materials for Cu(II) removal from aqueous solutions

| Adsorbent                                       | Reference                    | Cu(II) $C_s$ (mg/g) |
|---|------------------------------|---------------------|
| Calcareous soil (38% $CaCO_3$ ) (pH 5)          | Baghernejad et al., 2015     | 45.5                |
| Calcareous soil (27% $CaCO_3$ ) (pH 5)          | Baghernejad et al., 2015     | 50.0                |
| Calcareous clay (26.7% $CaCO_3$ ) (25 °C, pH 6) | Sdiri et al., 2014           | 27.39–17.88         |
| Calcareous soil (12% $CaCO_3$ ) (20 °C)         | Rodríguez-Rubio et al., 2003 | 6.93                |
| Calcareous soil (25 °C)                         | Echeverría et al., 1998      | 19.46               |
| Calcareous mudstone NTOL (25 °C, pH 5.5)        | This work                    | <b>103.24</b>       |

adsorption of ions at the calcite-water interface, ion-exchange reactions in the calcite surface monolayer, and the incorporation of trace elements into calcite (Heberling et al., 2014). Coprecipitation processes have been also described when the concentrations of trace elements are rather high (Gaskova et al., 2009; Perez-Sirvent et al., 2019).

As calcite is an important component of the NTOL calcareous mudstone, the differences between Cu(II) sorption capacities may be due to its affinity to the surface of calcite.

The precipitation of Cu(II) on the surface of sorbents is probable considering the dissolution of calcite under the conditions of this study. According to Al-Degs et al. (2006), the precipitation of heavy metals (M) as carbonate ( $MCO_3$ ) or hydroxycarbonate ( $M_2(OH)_2CO_3$ ) can occur in the presence of calcite. It can be calculated that the formation of metal hydroxycarbonates ( $M_2(OH)_2CO_3$ ) is not possible for Cu(II) under the experimental conditions of this study, as follows. Hydrolysis of Cu(II) ions by water can be presented as:



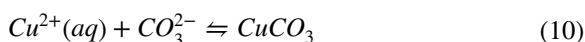
The equilibrium constant expression can be written as:

$$K_{a1} = \frac{[H^+][Cu(OH)^+]}{[Cu^{2+}]} \quad (8)$$

By calculating the value of  $[H^+]$  at equilibrium from the studied pH (5.5), and substituting the  $K_{a1}$  and  $H^+$  values into Eq. 8, the ratio  $[Cu^{2+}]/[Cu(OH)^+]$  is reduced to the following equation:

$$\frac{[Cu^{2+}]}{[Cu(OH)^+]} = 288 \quad (9)$$

This indicates that the concentration of free divalent  $Cu^{2+}$  is much higher than  $Cu(OH)^+$  at pH 5.5, therefore, the following reaction is more likely to occur:

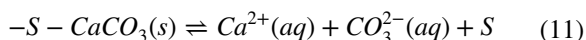


According to Harris (2010), the  $K_{sp}$  value for this reaction is  $2.3 \times 10^{-10}$ , thus, the minimum concentration of Cu(II) necessary to produce precipitation is 0.2 mg/L. Cu(II) equilibrium concentrations obtained

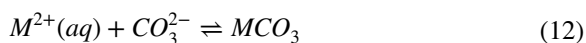
in this study exceed the maximum solubility value. Therefore, the presence of precipitated forms of  $CuCO_3$  is highly probable in all the studied concentration range and tests conditions.

Based on the above analysis, the sorption mechanism of metals by the calcite in the calcareous mudstone can be represented by the following surface reactions (Al-Degs et al., 2006):

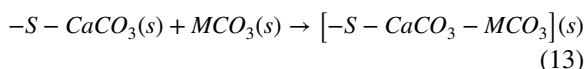
Dissolution of calcite that is present in the sorbent:



Interaction between the free metal ( $M^{2+}$ ) in solution and ( $CO_3^{2-}$ ) in solution can be described as:



Deposition of  $MCO_3$  on the sorbent surface:

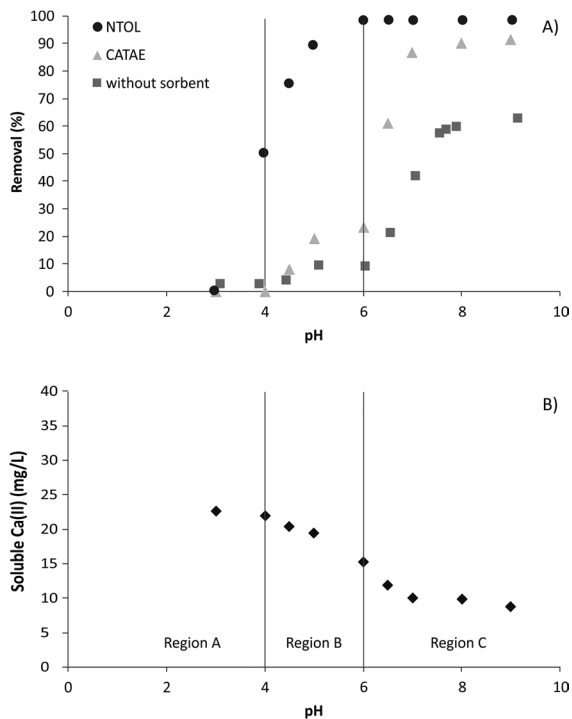


where  $M^{2+}$ ,  $-S-CaCO_3$ , and  $-S-CaCO_3-MCO_3$  stand for the free metal cation in solution, the surface active sites for adsorption, and the metal-carbonate complex on the sorbent surface, respectively.

### 3.4 pH Effect on Cu(II) Sorption

The effect of solution pH on Cu(II) removal for NTOL and CATAE is presented in Fig. 3. In order to elucidate the contribution of  $Cu(OH)_2$  chemical (or bulk) precipitation to the Cu(II) sorption, the change in removal percentage without the sorbent was examined under the same pH range. At pH lower than 6, the removal of Cu(II) from the solution by precipitation is lower than 10%, while at pH higher than 6, this percentage increases until a maximum value of 60% is reached at pH higher than 7.5. For the bentonite CATAE, a strong dependence of Cu(II) sorption with pH values was observed having low removal efficiency at low pH values which sharply increased at pH 6–7, and a constant maximum removal (90%) at  $pH > 7$  (Fig. 3A). Compared with the curve without sorbent, the shape is very similar to that and a beneficial effect of bentonite in removal can be considered at  $pH > 6.5$ . The difference between the total removal and the removal by precipitation at  $pH > 6.5$  is 30%, and this percentage could be attributed to the adsorption mechanism on the deprotonated aluminol and silanol groups of the clay, located at variable surface





**Fig. 3** Variation in removal percentages of Cu(II) as a function of pH (dose of adsorbent 1.24 g/L, ionic strength: 0.08 M, initial concentration of Cu(II): 2.5 mg/L) (A) and comparison between the removed Cu(II) by NTOL and calcium concentration of NTOL supernatants (B)

charged sites and on siloxanic groups located in permanent negative surface sites.

pH effect on Cu(II) sorption on NTOL was also evident but a very different pattern was observed. The curve can be divided into three regions (Fig. 3A). A region A ( $\text{pH} < 4$ ) where no removal is possible, a region B ( $\text{pH range} \leq 4$  to  $< 6$ ) where the removal efficiency is highly improved by the presence of the calcareous mudstone in a percentage between 50 and 80% more than the bentonite and the solution without the sorbent. Finally, a region C ( $\text{pH} > 6$ ) where the calcareous mudstone removes a 10% more than the bentonite CATAE, reaching a 100% of removal.

In region B, the presence of Ca(II) in solution, in NTOL supernatants, indicated that dissolution of calcite is possible between pH 4 and 6 (Fig. 3B). Ca(II) liberation in this zone could be presumably caused by Cu(II) sorption which involves surface replacement of Ca(II) by Cu(II) towards the formation of a Cu-bearing co-precipitate. Thus, in this region, the higher removal could be related to the precipitation

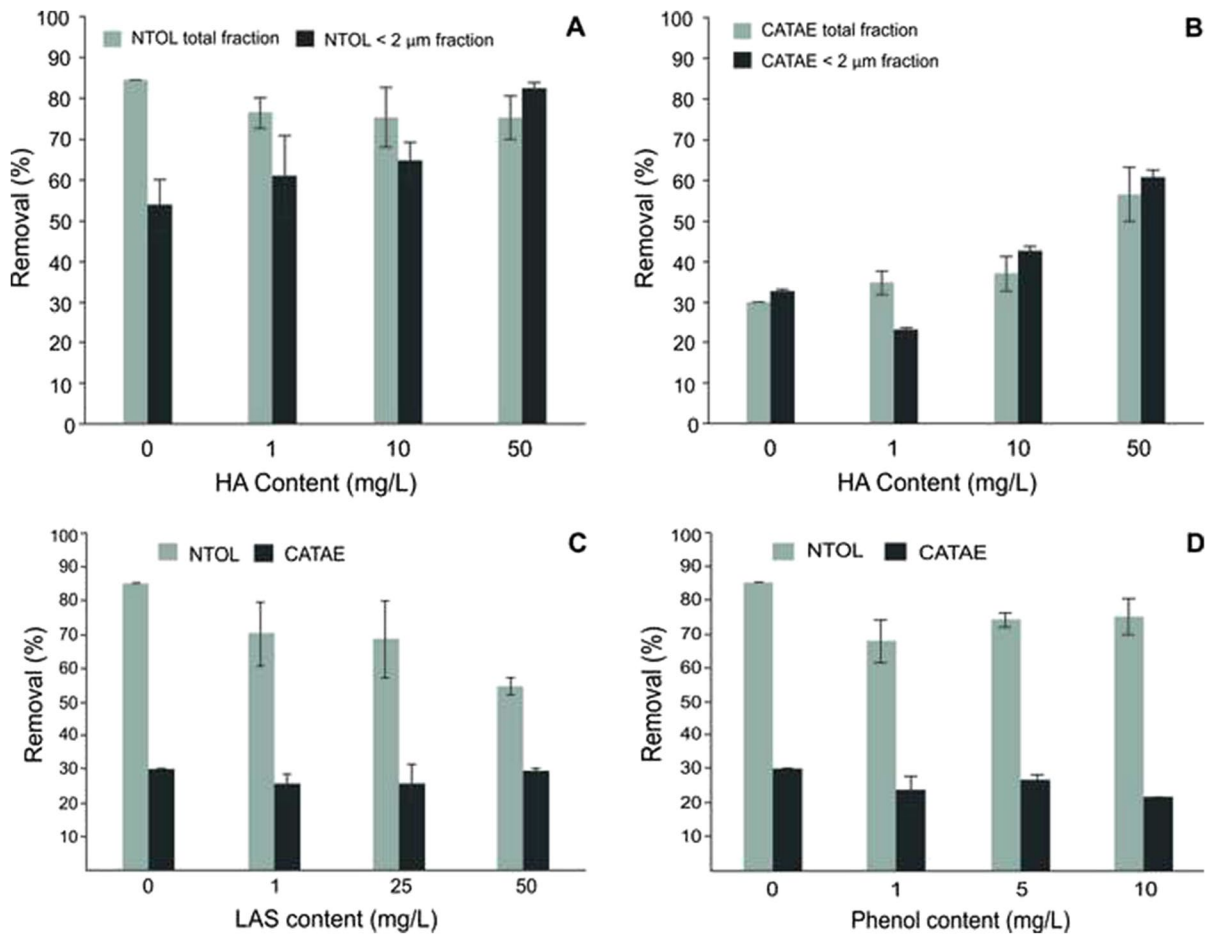
of compounds that can be formed due to the dissolution of calcite. Apart from precipitation on the surface of the calcite, a small metal quantity could be also retained via ion-exchange mechanism with the released Ca(II) from calcite (Elzinga et al., 2006; Heberling et al., 2011).

At  $\text{pH} > 6$ , the removal is very high but the concentration of Ca(II) in solution decreased. In this case, a 60% of removal is by chemical precipitation and the remaining could be attributed to adsorption mechanisms on the smectitic component of the I/S, favored by a higher external specific surface compared with CATAE bentonite (Table S1 in the supporting information), where a higher contribution of deprotonated aluminol and silanol groups of the clay, located at variable surface charged sites on the edges of clay particles, is possible.

### 3.5 Organic Compounds Effect on Cu(II) Sorption

In order to evaluate the influence of some organic compounds in the adsorption capacity of heavy metals by the calcareous mudstone, experiments including additions of HA, phenol, and surfactant to monometallic solutions of Cu(II) were performed. Figure 4A shows Cu(II) removal in the presence of HA for raw and clay fraction of NTOL calcareous mudstone. In the case of the total sample, Cu(II) removal decreased by 11% at 1 mg/L HA content and this value remained constant at higher HA contents. For clay fraction, Cu(II) removal increases as the HA content increased. When the HA concentration increased 10 times, an increment of 6% of the removal percentage was observed. When this concentration is 50 times the initial value, the removal increment arises to 26%. On the other hand, the capacity of the total sample and clay fraction of bentonite CATAE to remove Cu(II) ions in the presence of HA was the same. In this case, the percentage of removal increased with the increment of HA content (Fig. 4B).

The HA percentage retained by the calcareous mudstone and bentonite after equilibrium was 88% and 90%, respectively, showing a high interaction between HA and the clays (data not shown). The HA can form either inner sphere or outer sphere coordination complexes onto clay minerals through surface carboxylic and hydroxyl functional groups, hydrogen bond, and hydrophobic forces (Chen et al., 2017; Filius et al., 2000; Weng et al.,



**Fig. 4** Cu(II) removal effect in the presence of organic compounds. Cu(II) removal percentage in the presence of HA on calcareous mudstone NTOL (A) and bentonite CATAE (B); Cu(II) removal percentage in the presence of anionic surfactant

(LAS) (C); Cu(II) removal percentage in presence of phenol (D), pH 5.5,  $T=25\text{ }^{\circ}\text{C}$ , ionic strength 0.08 M, initial concentration of Cu(II) 3 mg/L

2006). At the same time, humic acids have been well known to exert strong effect on the sorption of heavy metal ions because of its high complexation ability (Chen et al., 2012; Tang et al., 2014; Yang et al., 2011). In this way, Cu(II) sorption could occur on the surface of the clay minerals or on the surface of the adsorbed HA. According to Jada et al. (2006), Cu(II) ion decreases HA surface charge promoting the formation of HA-Me complexes.

Cu(II) removal in NTOL clay fraction is favored in the same way than in CATAE clay fraction due to the probed affinity of HA with clay minerals. This is also valid for total sample of the bentonite which is also mainly constituted by smectite.

Anionic surfactant (LAS) effect on Cu(II) uptake was different for each material (Fig. 4C). In calcareous mudstone NTOL, the Cu(II) removal decreased in a 35% at high LAS concentration (50 mg/L). Other studies have demonstrated that anionic surfactants can be effectively sorbed by carbonates and  $\text{Ca}^{2+}$  montmorillonites (Ma et al., 2013; Yang et al., 2007). In calcareous mudstone NTOL, calcite and a  $\text{Ca}^{2+}$  smectitic I/S-mixed layer are present. Thus, the LAS could interact with these minerals decreasing the active sites available for sorption and co-precipitation of Cu(II).

In bentonite CATAE, the Cu(II) uptake for different LAS concentrations remained very similar than

the obtained without the presence of the surfactant. Adsorption of surfactant in hydrophilic minerals may result from a direct interaction between the solid surface and the adsorbate species due to electrostatic, chemical, or other forces (Ananthapadmanabhan & Somasundaran, 1985; Ou et al., 1996). Potential Z studies performed on bentonite CATAE indicated that this material has a very high density of negative charges at the studied pH (Musso et al., 2014). Therefore, it is expected that electrostatic repulsion occurs between the surface negative charge of the solid and the LAS. For this reason, this component would not interact with bentonite active sorption sites and the Cu(II) sorption would not be affected.

The Cu(II) uptake in calcareous mudstone and bentonite as a function of the concentration of phenol is shown in Fig. 4D. Within the experimental condition tested, the effect of the presence of phenol on both materials is quite similar, causing a slight decrease of Cu(II) removal (5–10%). Experiments of phenol binding to calcite and montmorillonites from aqueous solutions have demonstrated that this compound interacts with these minerals (Awad et al., 2019; Djebbar et al., 2012; Marcano et al., 2019). A decrease in the adsorption of Cu(II) ions with the increase of phenol concentration was observed by other studies, which have evaluated the competitive adsorption of phenol and Cu(II) onto a heat treated bentonite (Banat et al., 2001). However, in the experimental conditions of this study, phenol did not evidence a significant effect on Cu(II) removal.

### 3.6 Column Test Results

Commonly, the determination of transport adsorption parameters is achieved by using breakthrough curves (BTCs), which show the relationship between

the effluent concentration and time (Shackelford, 1994). The number of pore volume effluent (PVE) and testing time obtained from column test is shown in Table 3.

It can be observed the time consuming nature of this kind of tests and the low number of PVE obtained for both materials, especially for the bentonite CATAE which has the lowest hydraulic conductivity. The measured eluted concentration of Cu(II) from the PVE of NTOL filled columns was negligible (<0.1 mg/L). Physicochemical reactions between metals and NTOL particles produced a high retardation on the advancing front of contaminant inside the soil column. The magnitude of the calibrated sorption resulted very significant and therefore was not possible to determine the retardation factor in direct way. Then, retardation factor was computed from the calibrated Langmuir isotherm (Eq. 6) and then incorporated in the analytical solution of the advection–dispersion equation (Eq. 5). The calculated R values, considering the percentage of these clays in the columns were 3576 for NTOL and 113 for CATAE, demonstrating a greater ability of the calcareous mudstone to retain heavy metal mass during the transport in solution within the soil. Common retardation factors for other heavy metals observed in sand-bentonite mixtures are in the same order than the obtained here for CATAE (Chalermyanont et al., 2008).

Figure 5 presents the expected Cu(II) transport in the tested fixed-bed columns filled with NTOL according to Ogata and Banks (1961) (Eq. 5). Reactions between the metals in solution and NTOL particles are responsible for the negligible eluted concentration of Cu(II) indicating that the calcareous mudstone in the column did not reach its adsorption capacity. The oncoming front of heavy metals being transported through the column had

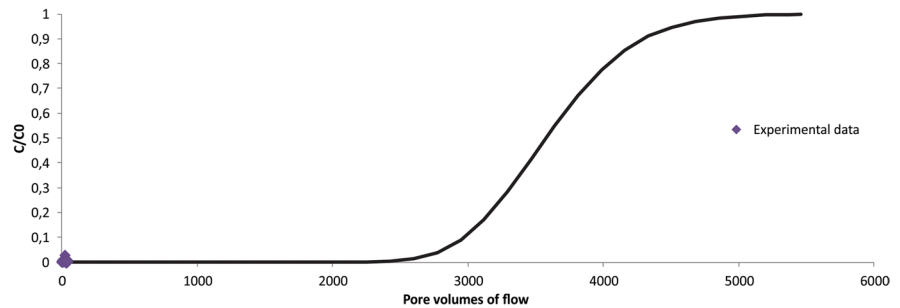
**Table 3** Hydraulic conductivity values (k), testing time (time in which the test is finished according to the criteria published in ASTM D5856-95 2007 norm) and pore volume effluent

| Column composition | Permeant fluid   | $k$ (m/s)*             | Std Dv                 | Testing Time (days)* | PVE* |
|--------------------|------------------|------------------------|------------------------|----------------------|------|
| NTOL 25%           | Deionized water  | $1.37 \times 10^{-10}$ | $3.91 \times 10^{-11}$ | 70                   | 1    |
|                    | Monometal Cu(II) | $4.67 \times 10^{-10}$ | $9.70 \times 10^{-11}$ | 365                  | 18   |
| CATAE 12%          | Deionized water  | $4.00 \times 10^{-11}$ | $5.82 \times 10^{-12}$ | 250                  | 1    |
|                    | Monometal Cu(II) | $2.50 \times 10^{-11}$ | $7.99 \times 10^{-12}$ | 507                  | 1    |

\* mean values

(PVE) of compacted sand-mudstones mixtures and sand-bentonite mixtures obtained from the column test

**Fig. 5** Model calculated Cu(II) breakthrough curve for compacted calcareous mudstone-sand mixtures filled column. The experimental conditions were as follows: column length 50 mm; column diameter 43 mm; hydraulic gradient 16–25; metal concentration 10 mg/L



very low displacement in the experimental time (365–490 days) given the retardation due to the sorption mechanisms demonstrated by means of batch tests. The expected percolation of the Cu(II) front is close to pore volume of effluent  $PVE = 3500$ , which is equivalent to 11 years.

Data shown in Fig. 5 indicate that a clay barrier constructed with NTOL calcareous mudstone would have a very good performance to restrict the displacement of Cu(II) metal ion.

#### 4 Conclusions

The results of this study indicate that the calcareous mudstone can be successfully used for Cu(II) ions removal from aqueous solutions. The kinetic studies indicated that the equilibrium for Cu(II) sorption was almost instantaneously revealing an ultrafast adsorption rate. This material, as it is extracted from the quarry, exhibited higher removal capacity in a wider pH range (4–9) than a commercial Na-bentonite which is a widely used heavy metal sorbent. The difference in the mineralogical composition of these materials would be the responsible for the higher Cu(II) removal capacity of the calcareous mudstone. In NTOL calcareous mudstone, calcite is present as an important constituent in the form of very small and highly porous calcareous nanofossils which contributed with the Cu(II) removal probably mainly through precipitation.

Cu(II) sorption was favored by the presence of humic acids in the clay fraction ( $< 2 \mu\text{m}$ ) of both materials revealing the high affinity of this compound with the surface of clay minerals and the subsequent formation of HA-Me complexes. The presence of an anionic surfactant or phenol slightly

affected the removal of Cu(II) indicating a low interaction of these compounds with the reactive minerals of the sorbents (calcite and smectite).

Column test results complemented the batch type experiments with a closer approximation to field conditions. In this study was observed that the period to breakthrough can be too long for materials with low hydraulic conductivities and high sorption capacity. Estimated retardation factor and numerical simulations of the expected Cu(II) transport in the tested fixed-bed columns filled with NTOL indicated that the migration of Cu(II) in the columns was significantly retarded by the calcareous mudstone. The extremely high retardation factor obtained for NTOL as raw material is in good agreement with the high adsorption capacity experimentally proved in batch tests. Calculated Cu(II) breakthrough curve indicated that Cu(II) ions would begin to percolate after 11 years of testing. The introduction of a calcareous mudstone in compacted clay barriers design is highly recommended to ensure long term retention of heavy metals.

**Author Contribution** Conceptualization: TM and LC. Methodology: LC, MEP, and FMF. Experiments: VL and MR. Interpretation: all authors. Writing original draft, review, and revision: TM. All authors have read and agreed to the published version of the paper.

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**Data Availability** The authors declare that all data supporting the findings of this study are available within the article (and its supplementary information files).

The authors have no conflict of interest to declare that are relevant to the content of this article. The authors declare data transparency. We applied the “sequence-determines-credit” (SDC) approach for the sequence of authors based on their declining contribution.

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