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$$\begin{aligned}
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 & \left\{ \begin{array}{l} \tau \\ \tau \end{array} \right. \left[ \begin{array}{l} \nabla \mathbf{v} \quad \nabla \mathbf{v} \quad - - (\nabla \cdot \mathbf{v} \quad -) \mathbf{I} \\ - - - (\nabla \cdot \mathbf{v} \quad -) \end{array} \right] \\
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 & \tau \quad \nabla \mathbf{v} \quad - \quad - \quad - \quad - \quad - \quad -
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 \tag{38}$$

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$$\begin{aligned}
 & \iint_{\Omega} \frac{\mathbf{v}}{\rho} \quad \iint_{\Omega} \left( \nabla \cdot \mathbf{g} - \tau \cdot \nabla \frac{\tau}{\rho} \right) - \int_{\Omega} \mathbf{n} \quad \int_{\Omega} \tau \cdot \mathbf{n} \\
 & \mathbf{n} \\
 & \mathbf{M} \iint_{\Omega} \frac{\mathbf{v}}{\rho} \quad \mathbf{M} \mathbf{A}_{\text{node}} \quad \mathbf{F}_{\text{node}} \\
 & \mathbf{A}_{\text{node}} \quad \mathbf{F}_{\text{node}}
 \end{aligned}$$

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$$\begin{aligned}
 & \mathbf{v}^{+1/2} \quad \mathbf{v}^{-1/2} \quad \mathbf{a} \\
 & \mathbf{x}^{+1} \quad \mathbf{x} \quad \mathbf{v}^{+1/2} \\
 & \mathbf{a}
 \end{aligned}$$

$$\left\{ \begin{array}{l} \frac{\partial}{\partial t} \left( \frac{1}{\rho} \nabla \cdot \mathbf{v} \right) - \frac{\partial}{\partial t} \left( \frac{1}{\rho} \nabla \cdot \mathbf{v} \right) \\ \frac{\partial}{\partial t} \left( \frac{1}{\rho} \nabla \cdot \mathbf{v} \right) - \frac{\partial}{\partial t} \left( \frac{1}{\rho} \nabla \cdot \mathbf{v} \right) \\ \frac{\partial}{\partial t} \left( \frac{1}{\rho} \nabla \cdot \mathbf{v} \right) - \left( \frac{\partial}{\partial t} \left( \frac{1}{\rho} \nabla \cdot \mathbf{v} \right) \right) \nabla \cdot \mathbf{v} - \end{array} \right.$$

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$$\frac{\partial}{\partial t} \left( \frac{1}{\rho} \nabla \cdot \mathbf{v} \right)$$

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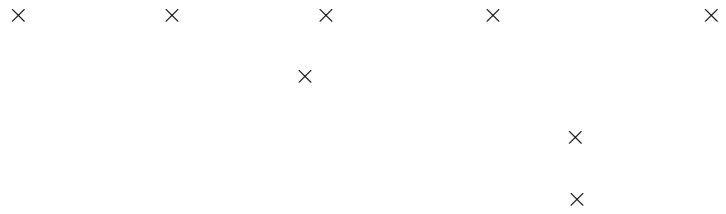
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$$\mathbf{v} \quad \mathbf{v} \quad -\mathbf{g} \quad - \quad \mathbf{v}$$

$$\cdot \quad \cdot \quad | \cdot |$$

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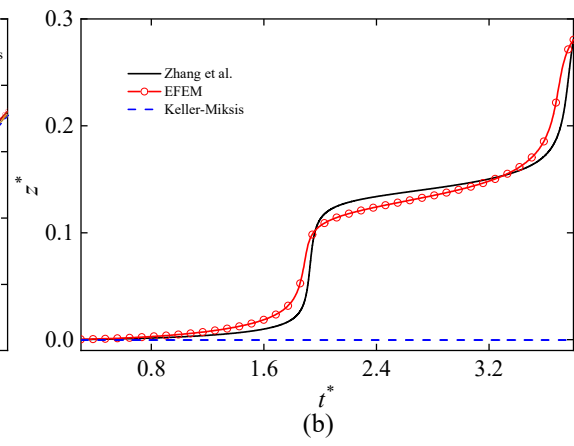
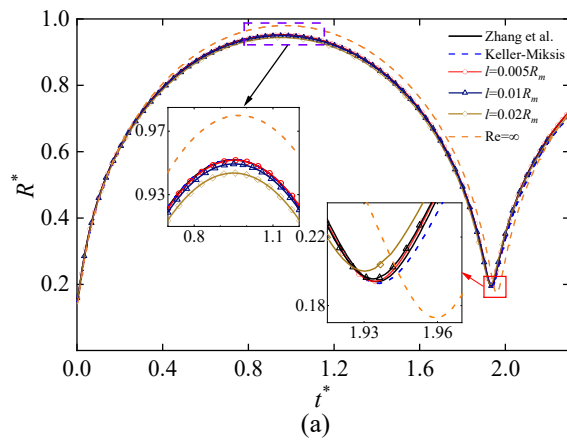
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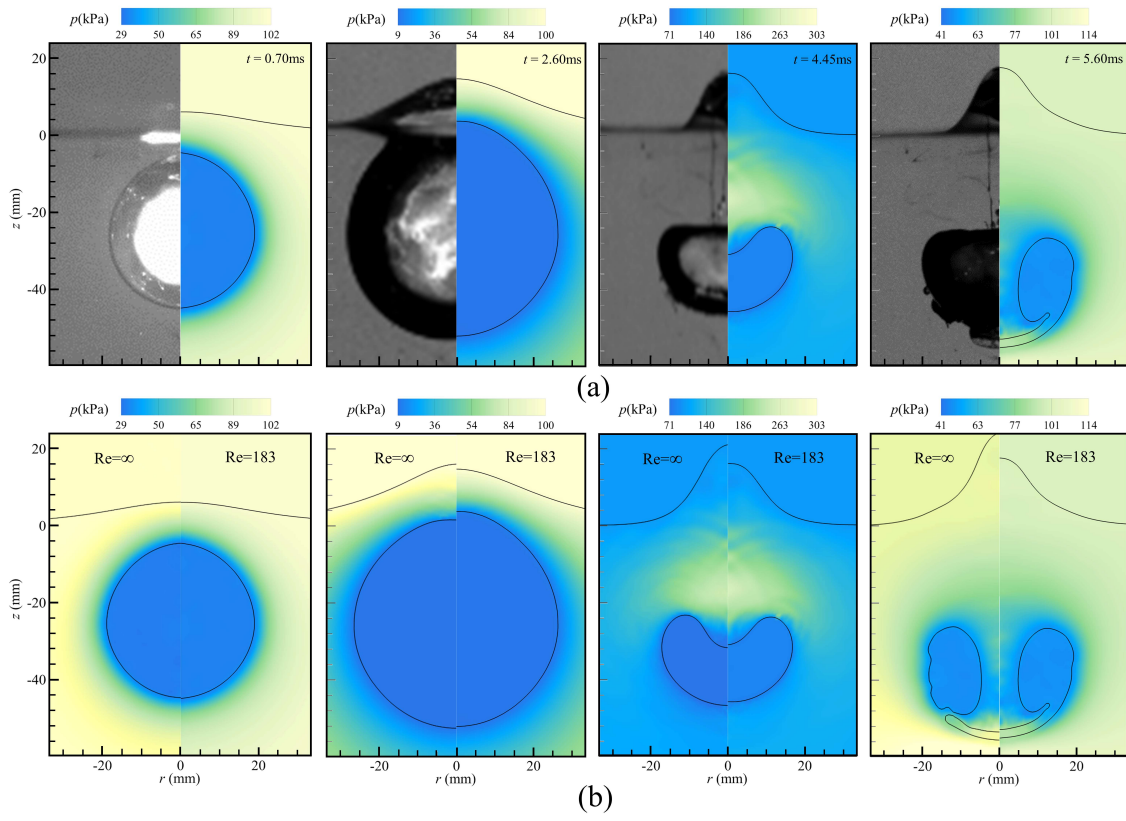
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Numerical analysis of nonlinear interaction between a gas bubble and free surface in a viscous compressible liquid



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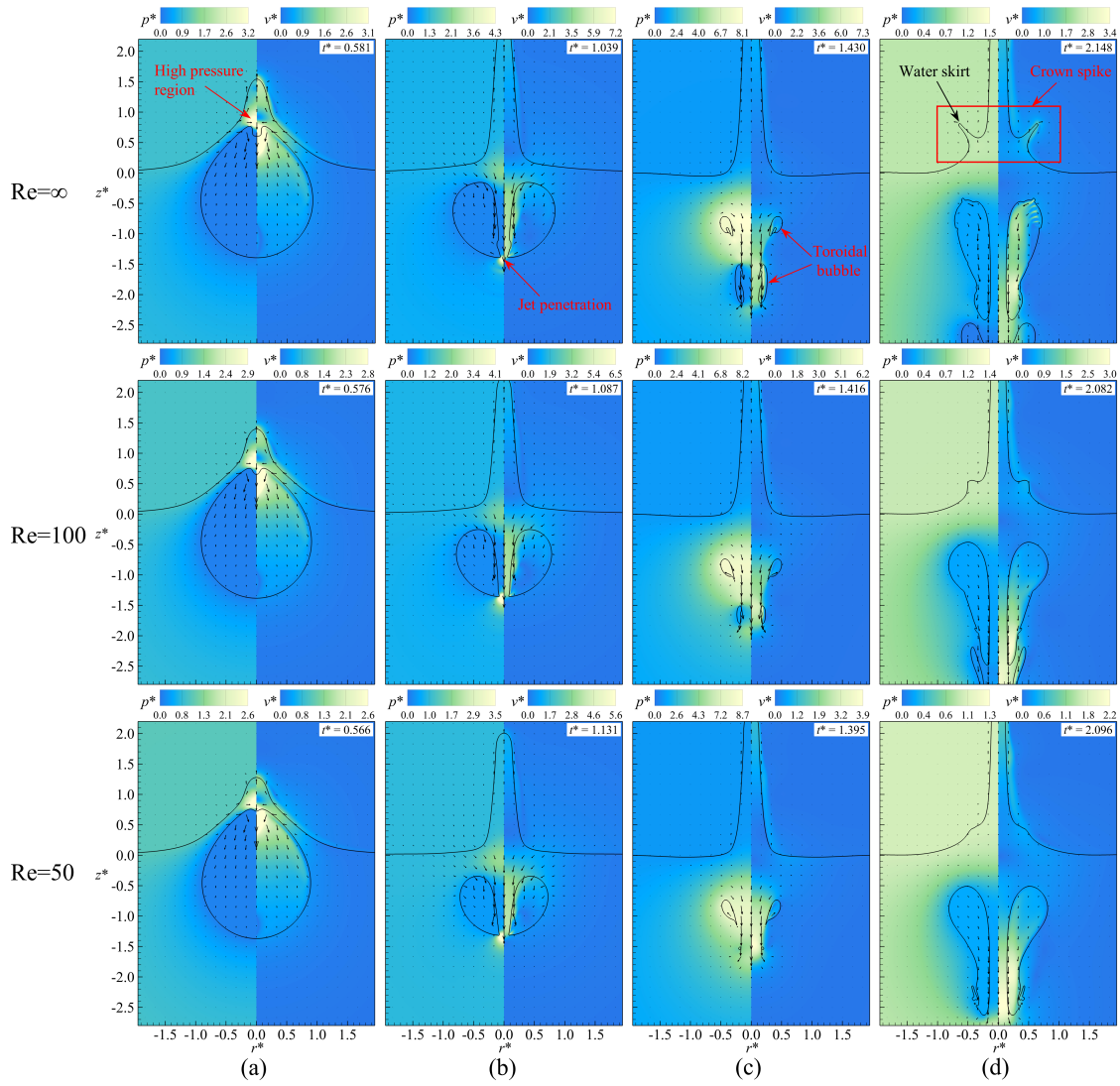
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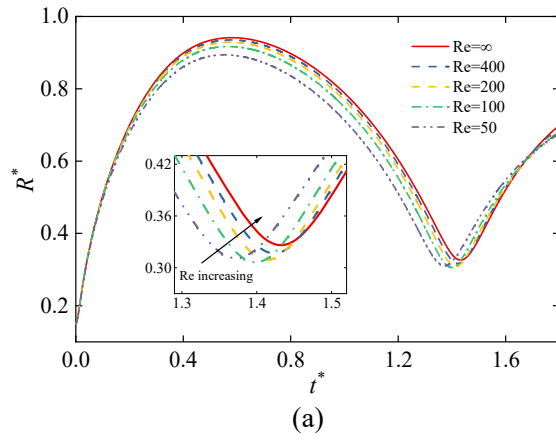
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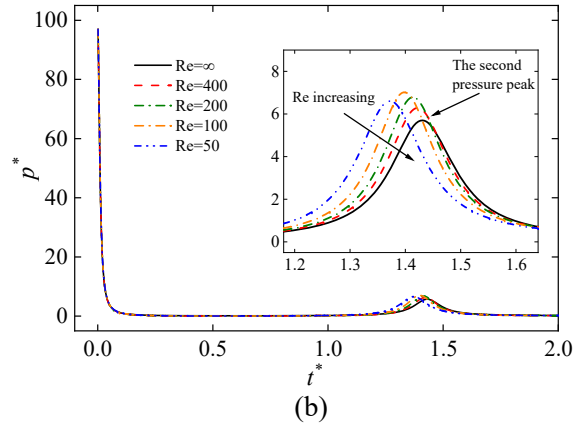




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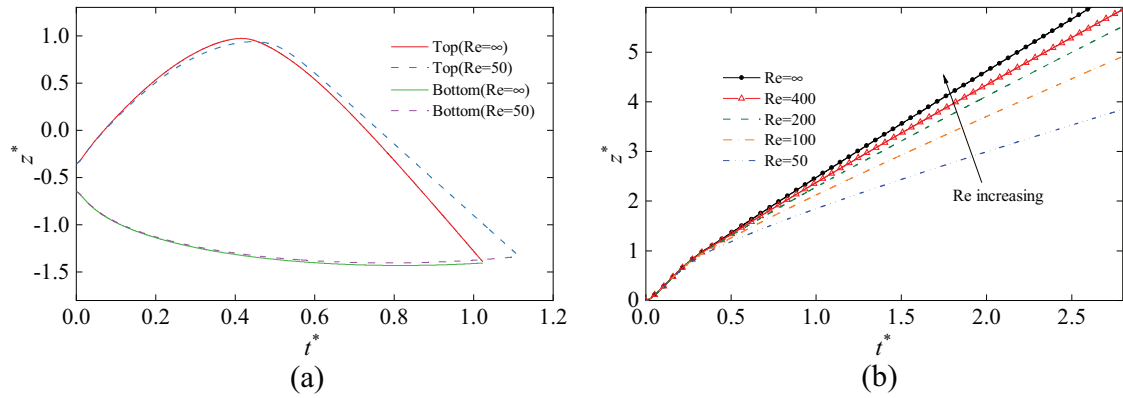


FIG. 6. Time histories of (a)the bubble top and bottom locations at  $Re = \infty$  and 50,  $\gamma_d = 0.5$ ; (b)the free surface spike height at different Reynolds numbers  $Re = 50, 100, 200, 400, \infty$ , and stand-off parameter  $\gamma_d = 0.5$ , respectively.

violently affected by the high-pressure region than the bottom. The jet penetrates the bottom at about  $t^* = 1.03$ , while the  $Re = 50$  bubble jet penetrates at  $t^* = 1.13$ . The slope of the displacement curve of the bubble in Fig.6(a) represents the jet velocity. It can be found that compared with the bubble with  $Re = 50$ , the jet velocity is faster without considering the viscosity of the liquid. Meanwhile, compared with Fig.4(a), it can also be found that the inviscid bubble has formed an obvious top jet before the bubble reaches the maximum volume.

The evolution of the free surface spike height at different Reynolds numbers is shown in Fig.6(b). In the initial expansion stage of the bubble, due to the relatively long distance from the free surface, the change of the free surface with different  $Re$  is the same. It can be seen from Fig.6(b) that as the  $Re$  decreases, the viscous effect increases and the height of the jet on the free surface decreases significantly. The main reason is the significant rate of change of tangential velocity caused by the jet, which leads to sizeable viscous friction and faster kinetic energy loss.

The pulsation of the bubble in the second period induces a low axisymmetric water skirt on both sides of the free-surface jet, called the crown spike. Fig.7(a) shows the shape of the crown spike under different Reynolds numbers  $Re$  when the bubble expands to the maximum volume in the second pulsation cycle. With the increase in Reynolds number, the phenomenon of a crown spike is more pronounced, and the height of the water skirt is also increasing. And the shape is sharp, and when  $Re = 50$ , the free surface almost does not form a crown spike, indicating that the viscous effect weakens the evolution of the free surface. Fig.7(b) shows the shapes of bubbles when jet impact with different Reynolds numbers. The  $Re = \infty$  bubble jet has a bulge at the front, called a mushroom-shaped jet. Koukouvinis<sup>26</sup> believes that the jet is caused by interface instability. However, compared with an inviscid bubble, the jet tip at the top of low Reynolds number bubbles is smoother, and no mushroom-shaped jet appears. Meanwhile, the volume of jet penetration is smaller, and the velocity and impact strength of the bubble jet is weak, which is reflected in the contours in Fig.4.

The bubble expands under the initial pressure. With the increase of liquid viscosity, the Reynolds number under the corresponding conditions decreases. The retardation effect of viscosity on bubble expansion becomes stronger and stronger, and the maximum radius of the bubble decreases. At the same time, the bubble jet is also affected by the viscosity, the jet velocity decreases with the decrease of the Reynolds number, and the jet penetration time is also delayed. The viscosity of the liquid affects the height and speed of the free surface jet: the viscosity increases, and the speed and height of the free surface jet decrease. When the viscosity increases to a specific value, the free surface crown spike generated by the pulsation of the bubbles will disappear, and the viscosity of the liquid weakens the interaction between bubbles and the free surface.

## B. Bubble dynamics with different stand-off parameters

In the same fluid, the viscosity coefficient of the liquid has been determined. When a pulsating bubble is generated using the same method, the effect of viscosity on bubbles is unchanged. The parameter that affects the dynamics of bubbles and the free surface is the distance  $d$  (as shown in Fig.1(a)), and the dimensionless parameter  $\gamma_d$  represents the inception depth of the bubble. Set  $Re = 100$ , other parameters remain the same

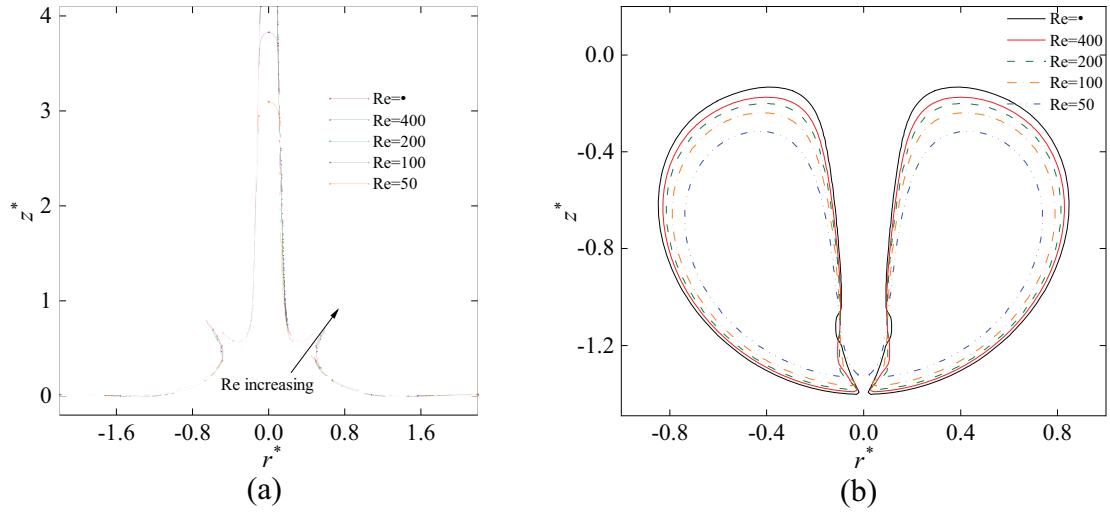
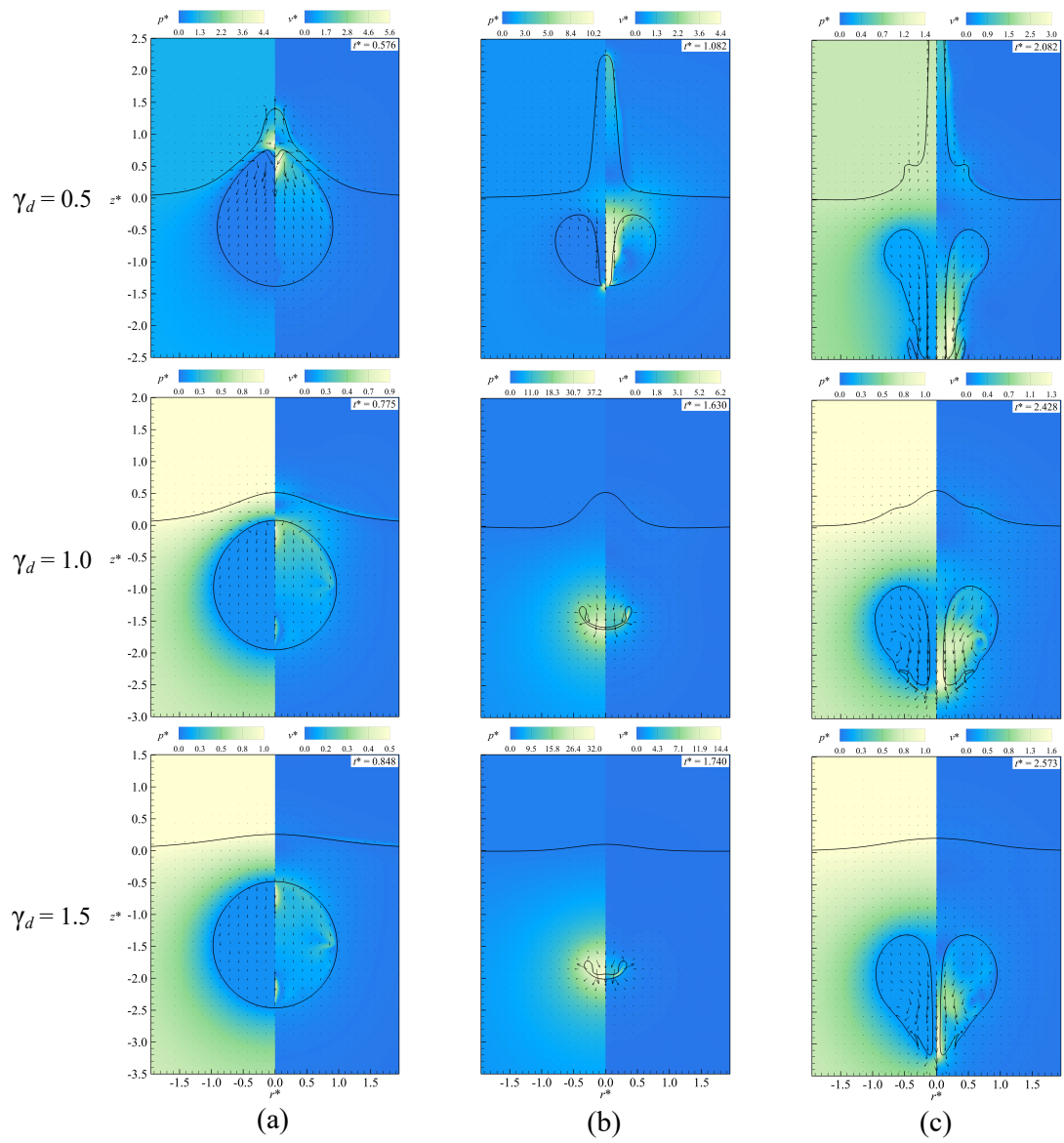


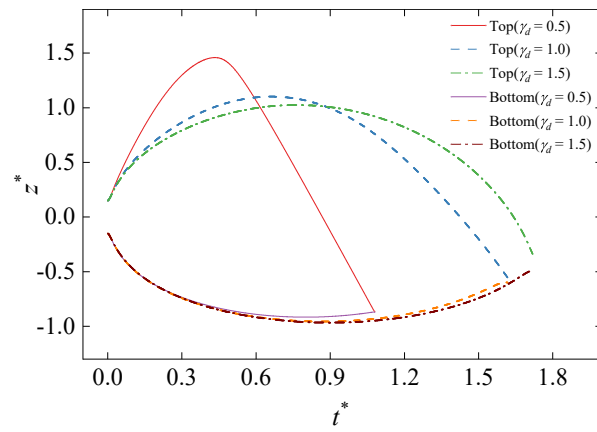
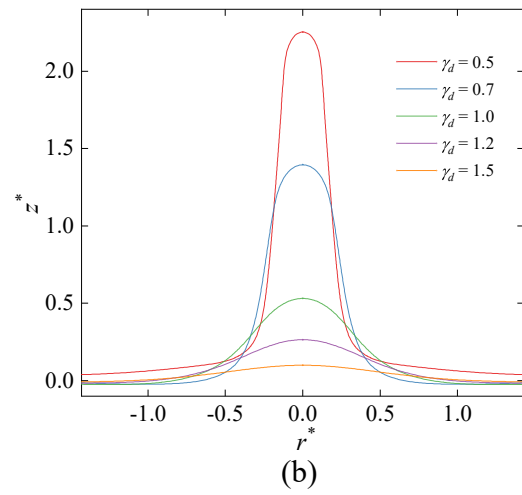
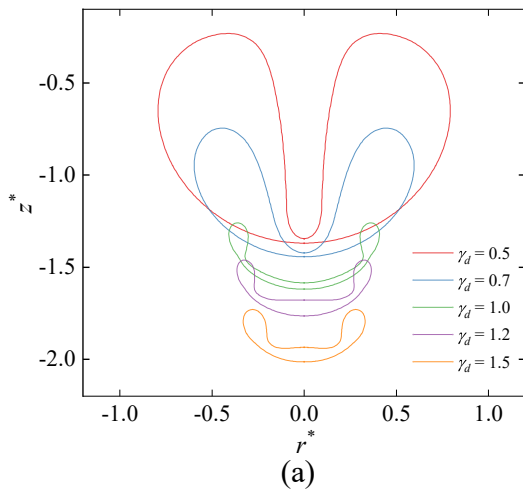
FIG. 7. (a)Shape of the free surface; (b)shape of the bubble when the jet impacts at different Reynolds numbers  $Re = 50, 100, 200, 400, \infty$ , and stand-off parameter  $\gamma_d = 0.5$ , respectively.

as the previous section, and study the bubble dynamics for  $\gamma_d = 0.5 - 1.5$ .

Fig.8 shows the bubble and the free surface shapes, pressure, and velocity contours at three important moments when Reynolds number  $Re = 100$  and stand-off parameter  $\gamma_d = 0.5, 1.0$  and  $1.5$ , respectively, corresponding to maximum bubble volume, jet impact, and maximum volume in the second pulsation period. The dimensionless time for the bubble to expand to the maximum radius increases with  $\gamma_d$ ,  $t^* = 0.576, 0.775$ , and  $0.848$ , respectively, as shown in Fig.8. The bubble jet is already formed in the expansion phase when  $\gamma_d = 0.5$ , while the bubble jet in the other two cases starts to form in the contraction phase. Compared with the other two conditions, the bubble and the free surface jet with smaller  $\gamma_d$  are also more slender, and the jet impacts the bottom earlier. As shown in Fig.8(b), bubble jets of  $\gamma_d = 1.0$  and  $1.5$  impacting the bottom occurred near the moment when bubbles collapsed to the minimum volume. In contrast, bubble jets of  $\gamma_d = 0.5$  had penetrated through the bottom in the contraction stage, and a local high-pressure region was formed when the jets penetrated through the bottom. It can be seen from Fig.8(c) that the bubble with  $\gamma_d = 0.5$  produces toroidal splitting because the jet penetrates the bottom earlier, and the annular sideways jet is generated when the bubble continues to collapse. This phenomenon is noticeable at large Reynolds numbers, and bubbles with larger stand-off parameters do not produce apparent toroidal splitting. At the same time, with the increase of  $\gamma_d$ , the free surface jet becomes lower, and the phenomenon of a crown spike is less obvious. The free surface does not produce a crown spike during the secondary pulsation of the bubble when  $\gamma_d = 1.5$ .

Fig.9(a) shows the shape of the bubble when the jet penetrates with different  $\gamma_d$ . It can be seen from the figure that with the increase of the stand-off parameter, the volume of bubble jet impact continues to decrease. When the inception depth is small, the impact time of the jet is earlier than the minimum volume time due to the strong interaction between bubbles and the free surface. The bubble jet width also varies with the change of the stand-off parameter. When the  $\gamma_d$  increases from  $0.5$  to  $1.0$ , the jet width gradually increases; when the  $\gamma_d$  increases from  $1.0$  to  $1.5$ , the jet width gradually decreases, which is the same as the law obtained by Li<sup>38</sup> without considering viscosity. With the increase of  $\gamma_d$ , the water jet penetration time is delayed, and the jet width changes due to the different degrees of bubble shrinkage. It can also be seen from the velocity contours in Fig.8(b) that the velocity of the jet impinges increases with the increase of  $\gamma_d$ . Fig.9(b) shows the shape of the free surface when the jet penetrates. With the increase of  $\gamma_d$ , the jet height of the free surface decreases while the jet width gradually increases. From the pressure contours in Fig.8(a), there is no high-pressure region below the free surface when the  $\gamma_d$  is large, which is not conducive to the generation of the bubble and the free surface jet. At the same time, the effect of bubble expansion on the free surface is weakened, which is also the reason for the low height of the free surface jet. Fig.10 shows the position changes of the top and bottom of the bubble on the axis, which can vividly see the changing trend of the axial length of the bubble. Meanwhile, the velocity of the bubble surface at the axis can also be obtained by calculating the slope of the curve. In the early stage of bubble expansion, the displacement of the upper surface of bubbles with different  $\gamma_d$  is different, and the displacement decreases with the increase





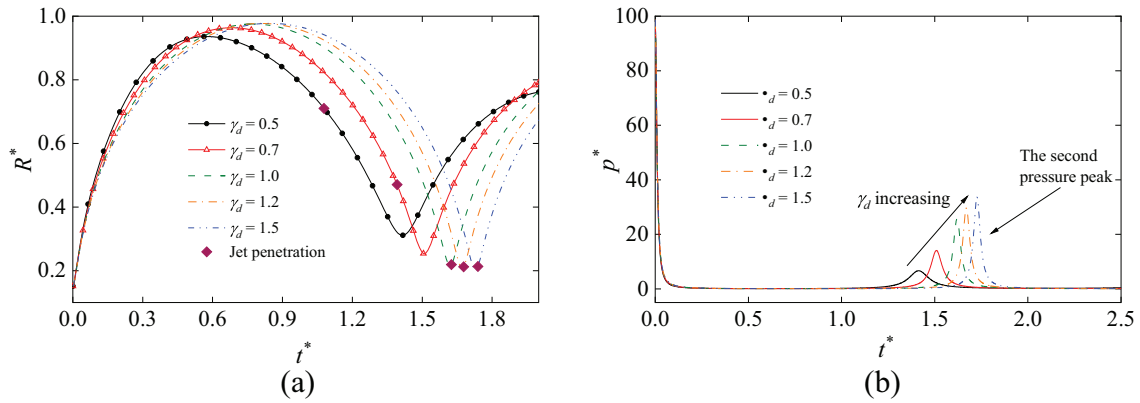


FIG. 11. Time histories of (a) the equivalent radius of bubbles; (b) average pressure in bubbles with different stand-off parameters  $\gamma_d=0.5, 0.7, 1.0, 1.2,$  and  $1.5$ ,  $Re=100$ , respectively.

- (I) As  $Re$  decreases, the bubble oscillation amplitude and period decrease, the bubble jet shape is blunter, the jet velocity decrease, and the impact time is delayed. At a lower  $Re$ , the jet is weaker and associated with less kinetic energy, resulting in earlier collapse. The viscosity also reduces the toroidal bubble splitting during pulsation, and the bubble with  $Re=50$  hardly splits.
- (II) As  $\gamma_d$  increases, the maximum bubble volume increases, the minimum bubble volume decreases, and the second pressure peak of the bubble increases. When  $\gamma_d$  decreases from  $1.5$  to  $0.5$ , the jet becomes sharper and impacts the opposite bubble surface earlier.
- (III) As  $Re$  decreases, the height and velocity of the free surface jet decrease, and the crown spike height decreases or even disappears in the second pulsation cycle. As  $\gamma_d$  increases, the free surface jet's height decreases, the jet's width increases, and the crown spike tends to be low or even disappear.

## ACKNOWLEDGMENTS

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