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Waste to treasure: Regeneration of porous Co-based catalysts from spent LiCoO₂ cathode materials for efficient oxygen evolution reaction

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8 catalysts from spent LiCoO_2 cathode materials for
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12 efficient oxygen evolution reaction
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47 **KEYWORDS:** spent Li-ion batteries, LiCoO_2 , Co_9S_8 , Co_3O_4 , oxygen evolution reaction
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3 ABSTRACT : The increasing demand for portable electronic devices and electric vehicles (EV)
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6 has triggered the rapid growth of rechargeable Li-ion batteries (LIBs) markets. However, in the
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8 near future, it is predicated a large amount of spent LIBs will be scrapped, imposing huge
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10 pressure on environmental protection and resources reclaiming. The effective recycling or
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12 regeneration of the spent LIBs not only relieves the environmental burdens but also avoids the
13
14 waste of valuable metal resources. Herein, a porous $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$ heterostructure is successfully
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16 synthesized from the spent LiCoO_2 (LCO) cathode materials via a conventional hydrometallurgy
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18 and sulfidation process. The fabricated $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$ catalyst proves high catalytic activity
19
20 towards oxygen evolution reaction (OER) in alkaline solution, with an overpotential of 274 mV
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22 to achieve the current density of 10 mA cm^{-2} and a Tafel slope of 48.7 mV dec^{-1} . This work
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24 demonstrates a facile regeneration process of Co-based electrocatalysts from the spent LiCoO_2
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26 cathode materials for efficient oxygen evolution reaction.
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32 SYNOPSIS: This study provides a facile strategy for regeneration of an efficient Co-based
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34 electrocatalyst towards electrochemical water splitting from the Li-ion batteries waste.
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44 INTRODUCTION

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47 As one of the most promising new energy techniques, rechargeable lithium-ion batteries (LIBs)
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49 have been widely used as energy storage devices, due to their high energy density, long cycle
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51 stability, low carbon emission and wide operating temperature.^{1, 2} In 2021, the global lithium
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53 market was estimated to be more than 400 kilotons lithium carbonate equivalent (LCE), and is
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3 expected to grow at a compound annual growth rate (CAGR) of 19.0% from 2022 to 2027.³ The
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5 soaring lithium market is mainly ascribed to the increasing demand for the LIBs in electric
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7 vehicles (EVs). In general, the lifespan of rechargeable LIBs is about 5-8 years,^{4, 5} after which
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9 the LIBs will eventually be scrapped. It has been estimated that the waste of the spent LIBs in
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11 vehicles is around 102,000 tons in 2020, which potentially reaches 7.8 million tons by 2040.⁶
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13 The spent LIBs not only contain some heavy metals but also toxic electrolytes (ethylene
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15 carbonate, lithium hexafluorophosphate and propylene carbonate etc.) and organic binders
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17 (polyvinylidene fluoride, PVDF)).⁷ Thus, the inappropriate disposal of spent LIBs may cause a
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19 series of environmental issues, including air pollution, groundwater pollution and damage to
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21 ecosystems, which finally endangers human health. Meanwhile, some valuable metals in LIBs,
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23 such as lithium, cobalt, nickel and manganese, are of great value in the trade market, for
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25 instance, the price of Li_2CO_3 is US\$78,502, Ni is US\$33,305 and Co is US\$82,160 per metric
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27 ton by April in 2022.⁸ With the growing demand for LIBs, the price of these battery raw
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29 materials is still increasing. Therefore, much attention needs to be paid for effective recycling
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31 and regeneration of spent LIBs, from the view of environmental protection and resource
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33 utilizations.
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42 Meanwhile, transition-metal-based compounds, especially the group VIII 3d metals of Fe,
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44 Co and Ni, are attractive as non-precious metal catalysts for electrochemical water oxidation
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46 reaction, due to their low cost, abundant resources, high activity, long-term durability and their
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48 excellent electronic properties.⁹⁻¹² For example, Zhang et al.¹³ fabricated a series of hierarchical
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50 Co_3O_4 hollow nanoplates doped with different metal atoms and found that Fe-doped Co_3O_4
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52 exhibited superior electrocatalytic properties for OER with an overpotential of 262 mV at 10 mA
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54 cm^{-2} . Wang et al.¹⁴ synthesized single-atomic Mo dispersed Co_9S_8 nanoflakes and the advanced
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3 catalyst exhibited pronounced water oxidation activities in universal pH conditions. Thus, the
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5 cathode materials of spent LIBs can be converted into Co-based, Ni-based or Fe-based catalysts
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7 for electrochemical water splitting via careful structure and composition design. In this work, we
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9 propose a novel strategy which combine conventional hydrometallurgy and sulfidation process to
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11 convert the spent LiCoO_2 (LCO) into porous $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$ heterostructures for efficient oxygen
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13 evolution reaction. In a typical hydrometallurgical process, the spent LCO was treated by oxalic
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15 acid and the extracted Co metals were precipitated in the state of cobalt oxalate (CoC_2O_4). The
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17 as-obtained CoC_2O_4 powders were then mixed with thioacetamide and annealed in Ar, resulting
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19 in a porous $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$ heterostructures. Benefiting from the hierarchical porous structure,
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21 $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$ catalyst exhibited outstanding OER activity with an overpotential of 274 mV at 10
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23 mA cm^{-2} , and a Tafel slope of 48.7 mV dec^{-1} . This work demonstrates an efficient strategy to
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25 recycle and regenerate the spent LCO batteries for electrochemical oxygen evolution reaction.
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35 EXPERIMENTAL SECTION

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38 **Preparation of porous Co_3O_4 , $\text{Co}/\text{Co}_3\text{O}_4$ and $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$.** The spent LCO LIBs were
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40 purchased from a portable source produced from a local new energy technology company
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42 (Hengchuang Co., Ltd, Shenzhen). Before manually dismantling, the spent LIBs were soaked in
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44 a 5 wt% NaCl solution to completely discharge and avoid short circuiting. The spent LCO
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46 materials were scratched and collected from the cathode, thoroughly rinsed by deionized (DI)
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48 water and ethanol several times, and then dried in oven. In a typical leaching process, the spent
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50 LCO was treated in a dilute oxalic acid (1.0 M) with a solid/liquid ratio of 4 g L^{-1} ,¹⁵ and then
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52 stirred under 200 rpm at 80 °C for 2 h. After that, CoC_2O_4 was precipitated and then filtered,
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3 dried in vacuum. For mesoporous Co_3O_4 , the obtained CoC_2O_4 was annealed in muffle furnace at
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5 350 °C for 2 h with a heating rate of 5 °C min^{-1} . For $\text{Co}/\text{Co}_3\text{O}_4$ fabrication, CoC_2O_4 was treated
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7 in $\text{N}_2/10 \text{ vol}\% \text{H}_2$ at 350 °C for 2 h with a heating rate of 5 °C min^{-1} . In a procedure to prepare
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9 $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$, CoC_2O_4 powder was mixed with thioacetamide (1/10, w/w) in Ar at 450 °C for 2 h
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11 with a heating rate of 5 °C min^{-1} .
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15 **Material characterization.** The morphology and structure of all the fabricated samples were
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17 examined by a field-emission scanning electron microscope (FEI PREO S(A5-112), transmission
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19 electron microscope (TEM, JEM-200 (JEOL)) and high-resolution transmission microscope
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21 (HRTEM) equipped with an EDX detector (Oxford INCA). Crystal structure of samples were
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23 recorded on a powder X-ray diffractometer (XRD, Rigaku) with $\text{Cu-K}\alpha$ radiation ($\lambda = 1.5405 \text{ \AA}$).
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25 Chemical composition and chemical state of the samples were analyzed by an X-ray
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27 photoelectron spectroscope (XPS, VG ESCALAB 220i-XL) with all the peak positions
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29 calibrated with respect to the $\text{C}1\text{s}$ peak at 284.8 eV. Thermogravimetric analysis (TGA) was used
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31 to confirm the stability and decomposition temperature of the fabricated CoC_2O_4 . N_2
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33 adsorption/desorption isotherms were recorded on a Quantachrome Nova 1200e Surface Area
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35 Analyzer at 77 K. Raman spectra were measured using a Renishaw 2000 Raman microscope
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37 with a laser wavelength of 532 nm.
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44 **Electrochemical measurements.** All the electrochemical activities were performed on a
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46 Metrohm Autolab electrochemical workstation in a conventional three-electrode setup, with the
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48 fabricated sample as the working electrode, a saturated Ag/AgCl as the reference electrode, a Pt
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50 foil as the counter electrode. For the working electrode fabrication, 5 mg of the catalysts were
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52 dispersed into a mixed solvent of 1 mL isopropanol/water (4:1 v/v) and 100 μL 5 wt % Nafion
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54 solution. The catalytic ink was then gradually dripped on the surface of carbon paper (CP) with a
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loading of $\sim 1.0 \text{ mg cm}^{-2}$, followed by drying under infrared lamp. 1 M KOH (pH=13.8) electrolyte was bubbled with high purity Ar gas before the test. All the tests were conducted at the room temperature. Before the measurement of the catalysts, cyclic voltammetry (CV) from 0 to 0.8 V (vs. Ag/AgCl) at 100 mV s^{-1} were tested for 20 cycles to activate the electrode. The linear sweep voltammetry (LSV) from 0 to 0.8 V with a scan rate of 2 mV s^{-1} was applied to evaluate the activity of the obtained materials. All the data were recorded with *i*R-correction. The electrochemical surface area (ECSA) was determined by CV measurements with various scan rates. The current density was normalized by ECSA according to the equation of $I_{\text{ECSA}} = I/S_{\text{ECSA}}$, where I = current density, I_{ECSA} = normalized current density and $S_{\text{ECSA}} = C_{\text{dl}}/C_s$ (C_{dl} = double layer capacitance, $C_s = 60 \text{ } \mu\text{F cm}^{-2}$). Electrochemical impedance spectroscopy (EIS) measurements were carried out with an amplitude of $\pm 5 \text{ mV}$ in the frequency range of 100 kHz - 0.01 Hz at the desired overpotential (η). The stability tests were performed by chronoamperometry measurements (I - t curves) at fixed overpotential over time. All potentials were converted to reversible hydrogen electrode (RHE) according to the equation below:

$$E (\text{vs RHE}) = E (\text{vs Ag/AgCl}) + 0.197 + 0.059 \times \text{pH} (= 13.8)$$

where E (vs Ag/AgCl) was the recorded potential vs. Ag/AgCl electrode.

RESULTS AND DISCUSSIONS

Fig. 1a shows the typical recycling and regeneration process of the spent LCO batteries to Co-based catalysts. First, the collected LCO powders were dispersed in hot oxalic solution (1 M, 80 °C) to extract the metal ions,¹⁵ i.e., Li^+ and Co^{2+} . The leaching efficiency of Li and Co was confirmed from the inductively coupled plasma-optical emission spectrometry (ICP-OES). From

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3 ICP-OES results shown in Fig. S1, the leaching efficiency of Li in the solution is over 98% after
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5 90 min, while extracted Co^{2+} would react with $\text{C}_2\text{O}_4^{2-}$ ions and precipitate in the state of CoC_2O_4 .
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7 Then, different annealing conditions were optimized for the target catalysts. Figs. S2 shows the
8
9 typical XRD patterns of the spent LiCoO_2 (JCPDS #50-0653, Fig S2a) and $\text{CoC}_2\text{O}_4 \cdot 2\text{H}_2\text{O}$
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11 powders (JCPDS #25-0250, Fig. S2b)). XRD patterns of the as-obtained catalysts (Figs. 1b, S6,
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13 S8 and S10) show a set of diffraction peaks at 19° , 31.3° , 36.8° and 44.8° , which are indexed to
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15 the (111), (220), (311) and (400) planes of Co_3O_4 (JCPDS #43-1003), respectively. The peak at
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17 44.3° is attributed to the (002) plane of Co (JCPDS #05-0727), while the peaks at 29.8° , 31.2° ,
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19 47.5° and 52.1° are associated to the (311), (222), (511) and (440) planes of Co_9S_8 (JCPDS #65-
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21 6801), respectively. SEM images demonstrate that the spent LCO powder shows granular
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23 structure with variable particle size (Fig. S3a), while the precipitated CoC_2O_4 powder exhibit
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25 typical orthorhombic crystal structure (Fig. S3b). When annealing in air, the CoC_2O_4 crystals
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27 gradually decompose to Co_3O_4 nanoparticles with an average particle size of 13.5 nm (Figs. 1c-
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29 d). When treated in $\text{N}_2/10\text{vol}\% \text{H}_2$, CoC_2O_4 is transformed into $\text{Co}/\text{Co}_3\text{O}_4$ nanoparticles with an
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31 average particle size of ~ 36.8 nm (Figs. 1e-f). Following the sulphuration process, the
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33 nanoparticle morphology is preserved but particle size reduced to ~ 19.6 nm in average (Figs.
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35 1g-h).

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43 TGA result shows a weight loss at around 200°C (Fig. S4), which is ascribed to the loss of
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45 crystal water in $\text{CoC}_2\text{O}_4 \cdot 2\text{H}_2\text{O}$.¹⁵ The observed weight loss at $\sim 300^\circ\text{C}$ is mainly due to the
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47 decomposition reaction of CoC_2O_4 to Co_3O_4 .¹⁵ Such results reveal that annealing temperature
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49 should be optimized for porous structure generation, as too high temperature would coarsen the
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51 structure and too low temperature would cause incomplete decomposition of CoC_2O_4 .
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53 Temperature-dependent experiment was also carried out in order to further evaluate the
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3 morphology and structure evolution during annealing in air and N₂/10vol% H₂. At low
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5 temperature in air (250 °C 2 h), lath-shaped microstructure is observed in some of regions (Figs.
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7 S5a-b). The lath structure is attributed to the incomplete decomposition of CoC₂O₄ crystals,
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9 which is also indicated from the corresponding XRD results (Grey line in Fig. S6). With
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11 gradually increasing the annealing temperature, the mean particle size of the sample increases
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13 from 13.5 nm at 350 °C (Fig 1d) to 50.4 nm at 650 °C (Figs. S5d-l). The phase structure of Co₃O₄
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15 can be confirmed from XRD patterns (Fig. S6). Similar phenomenon is observed when CoC₂O₄
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17 being treated in N₂/10 vol% H₂ (Fig. S7). The retained orthorhombic crystal morphology (Fig.
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19 S7a-b) and phase structure (Fig. S8) both suggest the presence of CoC₂O₄ at annealing
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21 temperature of 250 °C. At higher annealing temperature, all the samples show granular
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23 microstructures with mean particle size increasing from 36.8 nm at 350 °C (Fig 1f) to 610 nm at
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25 650 °C (Fig. S7d-l). XRD patterns show that Co₃O₄ is completely transformed to metallic Co
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27 phase at temperature higher than 450 °C (Fig. S8). To optimize the sulphuration parameters, the
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29 temperature and thioacetamide content are considered. Incomplete decomposition of CoC₂O₄ is
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31 observed at 350 °C (Fig. S10) with an average particle size of 17.1 nm (Fig S9a-c), while higher
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33 temperature at 550 °C incurs metallic Co phase (Fig. S10) and big particle size of ~ 120 nm (Fig.
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35 S9d-f). Co₉S₈ is formed with increasing the mixture of CoC₂O₄/thioacetamide (1/15, w/w) in Ar
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37 at 450 °C, exhibiting a hierarchical structure with an average size of 20.5 nm (Fig. 9g-i).
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46 The detailed morphology and microstructure of the samples were further investigated by
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48 transmission electron microscopy (TEM) and high-resolution TEM (HRTEM). As shown in Fig.
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50 2a-b, the prepared Co₃O₄ shows a mesoporous structure, which comprises of subunits with an
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52 average size of 12.3 nm, consistent with previous SEM observation. The clear lattice fringe of
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54 0.244 nm matches well with (311) plane of Co₃O₄ (Fig. 2c).¹⁶ For Co/Co₃O₄ and Co₉S₈/Co₃O₄,
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3 the mesoporous structure is also observed but with growing subunits (Figs. 2d-e and Figs. 2g-h).
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5 The lattice spacing of 0.244 nm, 0.155 nm and 0.216 nm correspond to the (311), (511) planes of
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7 Co_3O_4 , and (100) plane of Co, respectively.^{17, 18} A clear interface between Co and Co_3O_4 is
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9 observed, suggesting the Co is *in-situ* reduced on the surface of Co_3O_4 in $\text{N}_2/10$ vol% H_2 . The
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11 formed Co/ Co_3O_4 interface belongs to a typical Schottky junction, which can enhance the surface
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13 charge density of interfacial metals for improving the catalytic activity.¹⁹ For $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$, the
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15 lattice spacing of 0.30 nm, 0.175 nm and 0.20 nm are assigned to the (311), (440) planes of
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17 Co_9S_8 ,²⁰ and (400) plane of Co_3O_4 ,²¹ respectively. Clearly interface observed between Co_9S_8 and
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19 Co_3O_4 will accelerate the charge transfer across the interface and increase active sites, thus,
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21 contributing an improved electrocatalytic process.²² The dark-field TEM image and the
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23 corresponding energy dispersive X-ray (EDX) element mapping images were recorded to
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25 confirm the elements in the samples. For $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$, a uniform distribution of Co, S and O
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27 elements over the whole structure is observed (Figs. 2j-m), suggesting the presence of a
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29 homogeneous $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$ interface in the sample. The EDX mapping results of Co_3O_4 and
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31 Co/ Co_3O_4 also demonstrate the existence and distribution of Co and O in the sample, as shown in
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33 Fig. S11.
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41 The survey spectra of X-ray photoelectron spectroscopy (XPS) of Co_3O_4 and Co/ Co_3O_4
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43 (Fig. 3a) also confirm the existence of Co and O, while $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$ is composed of Co, S and
44
45 O. In the Co2p spectra of all samples, the peaks at 781.7 and 797.9 eV, 780.0 and 796.2 eV are
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47 reflected to Co $2p_{3/2}$ and $2p_{1/2}$ of Co^{2+} in Co_3O_4 , Co $2p_{3/2}$ and $2p_{1/2}$ of Co^{3+} in Co_3O_4 , respectively,
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49 while the peaks at 786.6 and 803.5 eV are accredited to the satellite peaks of Co^{2+} .²³⁻²⁵ For
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51 Co/ Co_3O_4 , two new peaks located at 778.1 and 794.0 eV are accredited to the Co $2p_{3/2}$ and $2p_{1/2}$
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53 spin orbitals of the Co^0 , respectively, due to the existence of metallic Co in the sample.²⁶ For
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3 Co₉S₈/Co₃O₄, the peaks with binding energies of 778.3 and 793.7 eV can be attributed to Co
4 2p_{3/2} and 2p_{1/2} from cobalt sulfides.^{27, 28} In the deconvoluted S 2p spectrum of Co₉S₈/Co₃O₄ (Fig.
5 3c), the peaks located at 162.0 and 163.6 eV can be assigned to S 2p_{3/2} and 2p_{1/2} of Co-S bonds
6 in Co₉S₈.¹⁴ The peak evolves at 168.8 eV can be ascribed to the oxidized S species (SO_xⁿ⁻),
7 implying easily surface oxidation of Co₉S₈ in air atmosphere.^{29, 30} As for the O 1s spectra (Fig.
8 3d), the raw curves can be peak-fitted into three peaks located at 530.1, 531.7 and 533.8 eV,
9 which can be assigned to the lattice oxygen (O_L) of Co-O, oxygen vacancies (O_V) and surface
10 adsorbed hydroxyl groups, respectively.^{24, 31, 32} In comparison to Co₃O₄, Co/Co₃O₄ and
11 Co₉S₈/Co₃O₄ show obvious higher peak intensity at 531.7 eV, implying the significant improved
12 concentration of O_V. The existence of O_V can provide unsaturated coordination sites for
13 accelerated charge transfer and enhanced conductivity of the catalysts, thus facilitating the OER
14 electrochemical performance.^{31, 32}

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32 The nitrogen adsorption-desorption isotherm curves of Co₃O₄, Co/Co₃O₄ and Co₉S₈/Co₃O₄
33 were depicted in Fig. 3e. All the curves show a typical Type IV characteristics with a hysteresis
34 loop, demonstrating the presence of porous structures in all samples. The BET (Brunauer-
35 Emmett-Teller) calculation indicates the Co₃O₄ has the largest surface area of 51.2 m² g⁻¹, while
36 Co/Co₃O₄ and Co₉S₈/Co₃O₄ exhibit a surface area of 20.9 and 34.7 m² g⁻¹, respectively. The
37 decreased surface area of Co/Co₃O₄ and Co₉S₈/Co₃O₄ may be ascribed to their increased
38 subunits. Besides, the pore size distribution was obtained by density functional theory (DFT)
39 method (Fig. 3f). All samples show mixed pores in the range of 15-100 nm, indicating the
40 hierarchical porous structure (mesopores and macropores) of the sample. The hierarchical porous
41 architecture with the heterojunction structure, has great influence on the mass and electron
42 transportation during electrochemical reactions. Compared to Co/Co₃O₄, some of pores below 15
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3 nm are observed for Co_3O_4 and $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$, which maybe another reason for a large surface
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5 area.
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8 The electrocatalytic OER performance of the recycled Co-based catalysts were evaluated in
9 a three-electrode cell in 1.0 M KOH. The polarization curves were tested by linear sweep
10 voltammetry (LSV) with a scan rate of 2 mV s^{-1} . As shown in Figs. 4a and S14a-b, $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$
11 exhibits the best catalytic performance with a η_{10} (overpotential to achieve the current density of
12 10 mA cm^{-2}) of 274 mV, which is lower than that of Co_3O_4 (342 mV), $\text{Co}/\text{Co}_3\text{O}_4$ (298 mV),
13 RuO_2 (293 mV), $\text{Co}/\text{Co}_9\text{S}_8$ (302 mV), Co_9S_8 (311 mV) and most of the reported Co-based
14 electrocatalysts in alkaline electrolyte (Fig. 4b and Table S1). At large current densities ($>50 \text{ mA}$
15 cm^{-2}), $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$ also displays remarkable OER performance. It delivers a η_{100} (overpotential
16 to achieve the current density of 100 mA cm^{-2}) of 335 mV, which is much lower than that of
17 Co_3O_4 (417 mV), $\text{Co}/\text{Co}_3\text{O}_4$ (362 mV) and RuO_2 (390 mV). It is also notable that $\text{Co}/\text{Co}_3\text{O}_4$
18 exhibits better catalytic performance than RuO_2 at high current density ($>50 \text{ mA cm}^{-2}$), which
19 may be ascribed to the hierarchical porous architecture and presence of Schottky junction in
20 $\text{Co}/\text{Co}_3\text{O}_4$. The electrocatalytic OER activity of air-treated and $\text{N}_2/10 \text{ vol}\% \text{ H}_2$ -annealed samples
21 at 250-650 °C, thioacetamide-treated samples at 350 and 550 °C, and Co_9S_8 were also evaluated,
22 as shown in Figs. S12-14. The sample treated in air and $\text{N}_2/10 \text{ vol}\% \text{ H}_2$ at 350 °C exhibits the best
23 OER performance, either too low or too high annealing temperature would deteriorate the
24 catalytic performance of the electrode. Similar result is also observed for thioacetamide-treated
25 sample at 350-550 °C (Fig. S14). The Tafel slope derived from LSV curve was also applied to
26 evaluate the OER kinetics of prepared samples (Figs. 4c and S14c). The $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$ shows the
27 lowest Tafel slope with a value of 48.7 mV dec^{-1} , while Co_3O_4 , $\text{Co}/\text{Co}_3\text{O}_4$, RuO_2 , CP (carbon
28 paper), $\text{Co}/\text{Co}_9\text{S}_8$ and Co_9S_8 exhibit a Tafel slope of 70.5, 58.6, 57.6, 187.6, 62.9 and 78.1 mV
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3 dec⁻¹, respectively. The lower Tafel slope of Co₉S₈/Co₃O₄ suggests the faster OER kinetics than
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5 Co₃O₄, Co/Co₃O₄, RuO₂, CP, Co/Co₉S₈ and Co₉S₈.
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9 To better understand the OER activity of the prepared samples, the electrochemical active
10 surface area (ECSA) was evaluated by electrochemical double layer capacitance (C_{dl}) based on
11 the cycle voltammetry (CV) curves at different scan rates. Fig. 4d shows the CV curves of
12 Co₉S₈/Co₃O₄ measured in the potential range of 0.875-0.975 V (vs. RHE) with a scan rate from
13 0.01 to 0.1 V s⁻¹. The C_{dl} of Co₉S₈/Co₃O₄ is calculated to be 12.5 mF cm⁻², which is nearly 3
14 times higher than that of Co/Co₃O₄ (4.8 mF cm⁻²) and about 6 times higher than that of Co₃O₄
15 (2.1 mF cm⁻²) and RuO₂ (2.4 mF cm⁻²) (Fig. 4e). Figs. S15-S16 show the CV curves of air-
16 annealed and N₂/10 vol% H₂-annealed samples and their corresponding ECSA results. It is
17 clearly observed that the samples annealed at 350 °C both in air and N₂/10 vol% H₂ show the
18 largest C_{dl}, either higher or lower annealing temperature result in a lower C_{dl}. The CV curves and
19 corresponding ECSA results also confirm the higher C_{dl} of Co₉S₈/Co₃O₄ than that of Co₉S₈ and
20 Co/Co₉S₈ (Fig. S17). It should be mentioned that the surface area (BET results) is not consistent
21 with the ECSA results, which is probably associated with the heterostructures in Co/Co₃O₄ and
22 Co₉S₈/Co₃O₄. Heterostructured catalysts usually possess more active sites than their single
23 counterpart.³³ Furthermore, the ECSA-normalized LSVs were plotted (Fig. S18) and the results
24 also demonstrated the higher intrinsic activity in Co₉S₈/Co₃O₄.
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46 Electrochemical impedance spectroscopy (EIS) was applied to evaluate the electron transfer
47 kinetics of the catalysts. Fig. 4f shows the Nyquist plot fitted with an equivalent circuit (inset in
48 Fig. 4f) of Co₃O₄, Co/Co₃O₄ and Co₉S₈/Co₃O₄. A unified electrolyte solution resistance (R_s) of
49 3.5-5 Ω is observed for all samples. Co₉S₈/Co₃O₄ shows a fitting charge transfer resistances (R_{ct})
50 of 34.7 Ω, which is much lower than that of Co₃O₄ (60.4 Ω) and Co/Co₃O₄ (121 Ω). The low R_{ct}
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3 value of $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$ indicates an excellent OER kinetics and a high charge-transfer rate at the
4 electrolyte/catalysts interface. Chronoamperometry at an overpotential of 300 mV was conducted
5 to examine the electrochemical stability of $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$ (Fig. 4g). The sample clearly shows a
6 steady state up to 20 h of the measurement. The surface morphology maintains after cycling test
7 (inset SEM image in Fig. 4g), suggesting the structure stability of $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$. Furthermore, the
8 long-term durability of $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$ was also evaluated by CV tests in a potential range of 0.8-
9 2.0 V (*vs.* RHE) at a scan rate of 0.1 V s^{-1} . After 1000 cycles, no obvious shift or shape change of
10 CV curves is observed, suggesting the high durability of the sample. Closely CV observation
11 shows an oxidation peak at $\sim 1.52 \text{ V}$, which can be ascribed to the reconstructed Co^{4+} species on
12 the surface of $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$.³⁴ The Raman spectrum of $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$ after CV cycling test shows
13 a broad peak at 576 cm^{-1} (Fig. S19), suggesting the presence of CoO_2 species.^{34, 35} The peaks at
14 610 cm^{-1} and 472 cm^{-1} can be ascribed to Co_3O_4 and Co_9S_8 , respectively.^{11, 36} For Co_3O_4 ,
15 $\text{Co}/\text{Co}_3\text{O}_4$ and Co_9S_8 , CV cycling curves show a bit shift indicating a less stable structure of
16 these catalysts (Figs. S20a, d and g). The peaks at 1.47 V and 1.37 V corresponding to the
17 oxidation of Co from $\text{Co}^{2+}/\text{Co}^{3+}$ and $\text{Co}^{3+}/\text{Co}^{4+}$ can be observed in the CV cycling curves,
18 suggesting the in-situ formation of CoOOH and Co^{4+} species on the surface of Co_3O_4 and
19 $\text{Co}/\text{Co}_3\text{O}_4$, respectively.^{34, 37} CV curves of Co_9S_8 exhibit anodic peaks at 1.15 V and 1.37 V due
20 to the oxidation of Co^+ to Co^{2+} and Co^{2+} to Co^{3+} , respectively. The CV result indicates the in-situ
21 formation of $\text{Co}(\text{OH})_2$ on the surface of Co_9S_8 , and further reconstructed to CoOOH before the
22 OER process. As shown in Figs. S20c, f and i, the Raman bands located at 465 (464 cm^{-1}) and
23 $673 (664 \text{ cm}^{-1})$ demonstrate the presence of CoOOH in the Co_3O_4 , $\text{Co}/\text{Co}_3\text{O}_4$ and Co_9S_8 .³⁸
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52 The exceptional OER performance of $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$ can be assigned to the synergetic effect
53 of the diverse porous architecture and heterojunction structures. On the one hand, the diverse
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3 porous architecture contains macropores and mesopores, where macropores provide quick
4 pathways for reactant and product, and mesopores can contribute more active sites on the
5 surface. On the other hand, the intimate combination of Co_9S_8 and Co_3O_4 lead to the formation of
6 a heterojunction interface, which is favorable for generating active sites as well as the fast charge
7 transport.^{39, 40} The interference between two different components induces interfacial electron
8 redistribution and tune the surface charge state, which promotes the OER dynamic kinetics.⁴¹
9 Importantly, fast charge transport induced by heterostructure will stimulate and stabilize Co^{4+}
10 species (CoO_2) on the surface of $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$, which can reduce the energy barrier of the
11 potential-determining step and thereby enhance the OER performance.³⁴ In addition, the
12 presence of abundant oxygen vacancies (O_V) in $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$ can modify the
13 absorption/desorption of electrocatalysts with the reactants as well as the electronic structure and
14 electronic conductivity of the catalysts, thus promoting the OER activities.⁴²
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34 CONCLUSION

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37 To sum up, a facile hydrometallurgy and thermal treatment were applied to regenerate Co-based
38 electrocatalysts from spent LCO cathode materials. Thermal temperature and atmosphere are
39 optimized to control the microstructure and composition of the Co-based catalysts. As a result,
40 $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$ obtained via a sulfidation process (450 °C, 2h) exhibited desirable OER activities
41 ($\eta_{10}=274$ mV, Tafel slope=48.7 mV dec⁻¹), outperforming Co_3O_4 ($\eta_{10}=342$ mV, Tafel slope=70.5
42 mV dec⁻¹), $\text{Co}/\text{Co}_3\text{O}_4$ ($\eta_{10}=298$ mV, Tafel slope=58.6 mV dec⁻¹) and even the commercial RuO_2
43 ($\eta_{10}=293$ mV, Tafel slope=57.6 mV dec⁻¹). The enhanced OER performance can be mainly
44 ascribed to the hierarchical porous architecture and heterojunction structures, which provide
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3 enhanced active sites for boosting reaction kinetics. This study demonstrated an appropriate
4 strategy for designing effective catalysts from the battery waste. Additionally, the successful
5 regeneration of Co-based materials not only saves the valuable Co and Li resources, but also
6 reduce environmental pollution.
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16 ASSOCIATED CONTENT

17 18 19 **Supporting Information.**

20 The Supporting Information is available online or from the author.

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24 ICP of Li leaching efficiency, SEM images and XRD patterns of air-annealed, N₂/10 vol% H₂-
25 annealed and thioacetamide-treated samples, LSV curves, CV curves, ECSA results and Raman
26 spectra of air-annealed, N₂/10 vol% H₂-annealed and thioacetamide-treated samples
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35 **Author Contributions**

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37 H. Bian designed the idea, carried out the experiments and wrote the paper. Z. Zhang, X-Y Lu
38 and C. Liu supervised the experiment. W. Wu, X. Liao and J. Xu helped the material
39 characterization and analysis. Y. Zhu helped dismantle the LIBs and electrode materials
40 fabrication. C. Tsang and X-Y Lu revised the paper. All authors discussed the results and
41 comments the manuscript.
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50 **Notes**

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53 The authors declare no conflict of interest.
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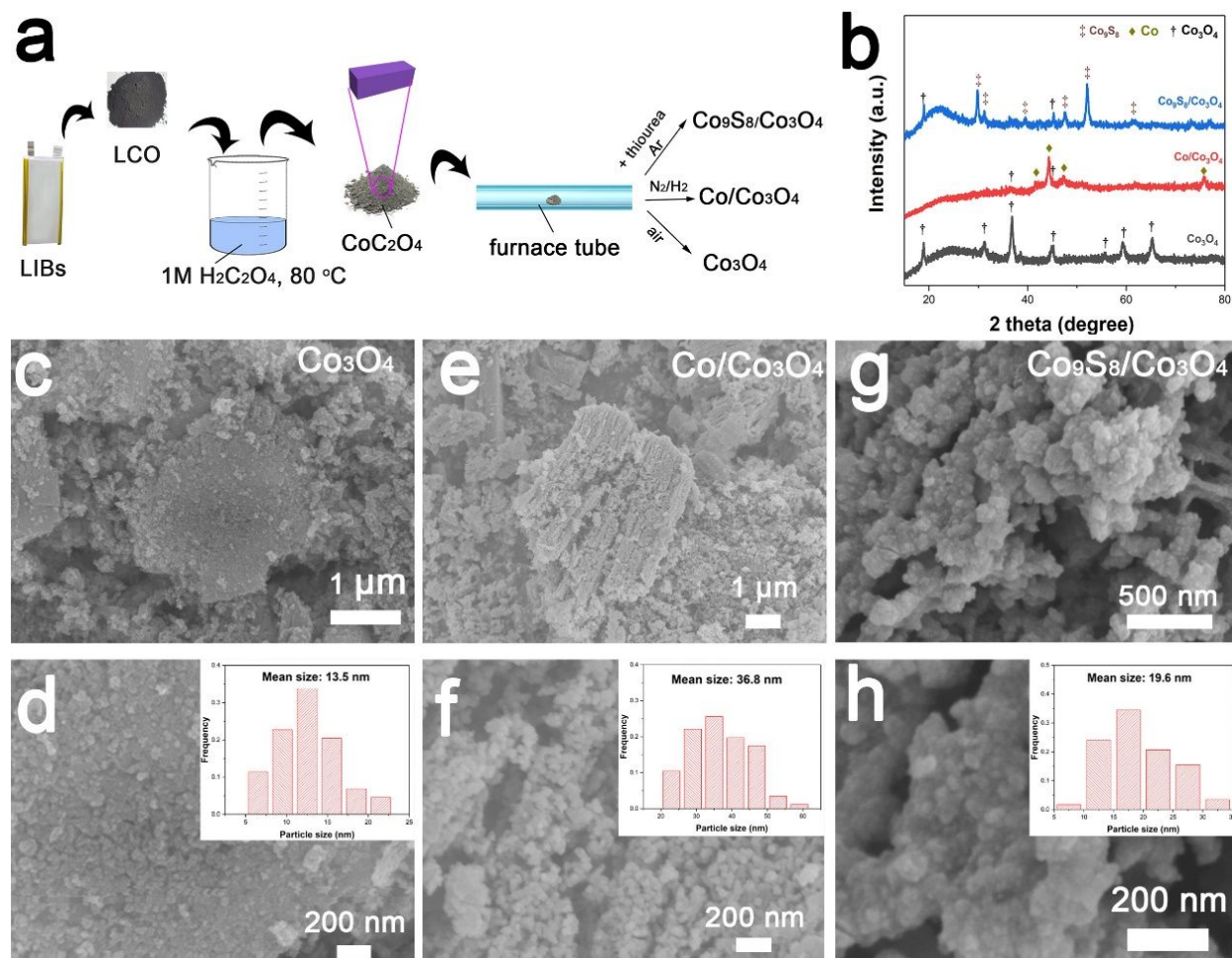


Fig. 1 a) Schematic illustration of recycling process of the spent LCO batteries to Co-based catalysts (Co_3O_4 , $\text{Co}/\text{Co}_3\text{O}_4$ and $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$); b) XRD patterns of the prepared Co_3O_4 , $\text{Co}/\text{Co}_3\text{O}_4$ and $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$; SEM images of c-d) Co_3O_4 , e-f) $\text{Co}/\text{Co}_3\text{O}_4$ and g-h) $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$ at different magnifications. The insets show the statistic particle size of the corresponding samples.

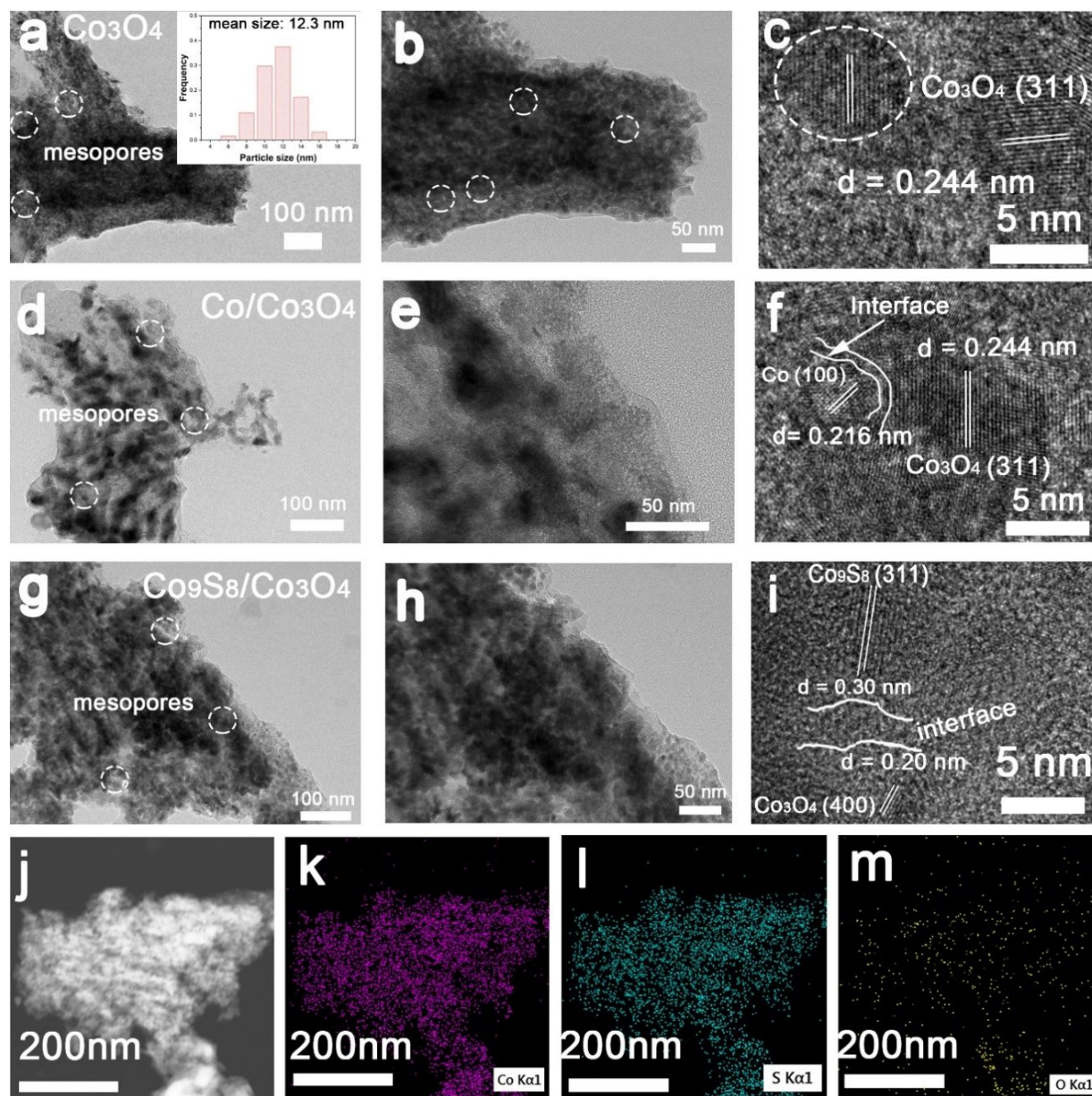


Fig. 2 TEM images of a-b) Co_3O_4 , d-e) $\text{Co}/\text{Co}_3\text{O}_4$ and g-h) $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$, HRTEM images of c) Co_3O_4 , f) $\text{Co}/\text{Co}_3\text{O}_4$ and i) $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$, and j-m) TEM image and elemental mapping images of $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$.

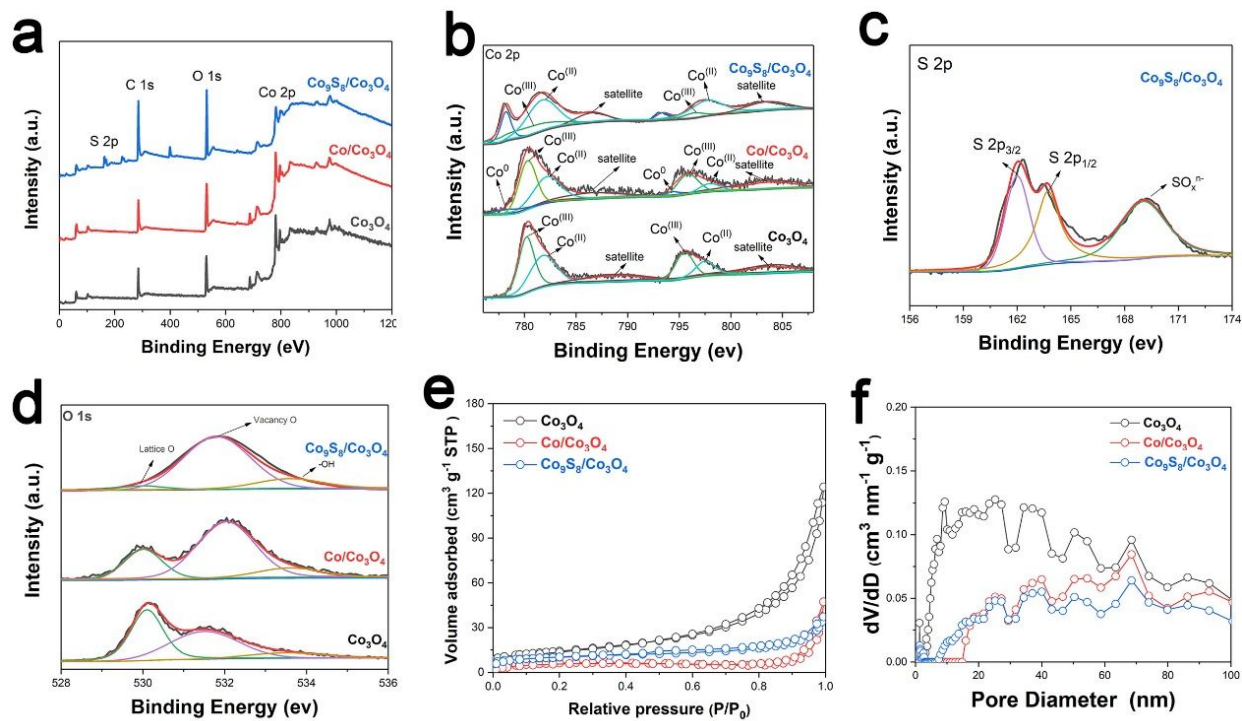


Fig. 3 a) XPS survey spectra, high-resolution Co2p (b), S2p (c) and O1s (d) XPS spectra, e) nitrogen adsorption-desorption isotherms and f) the corresponding pore size distribution of the prepared Co_3O_4 , $\text{Co}/\text{Co}_3\text{O}_4$ and $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$.

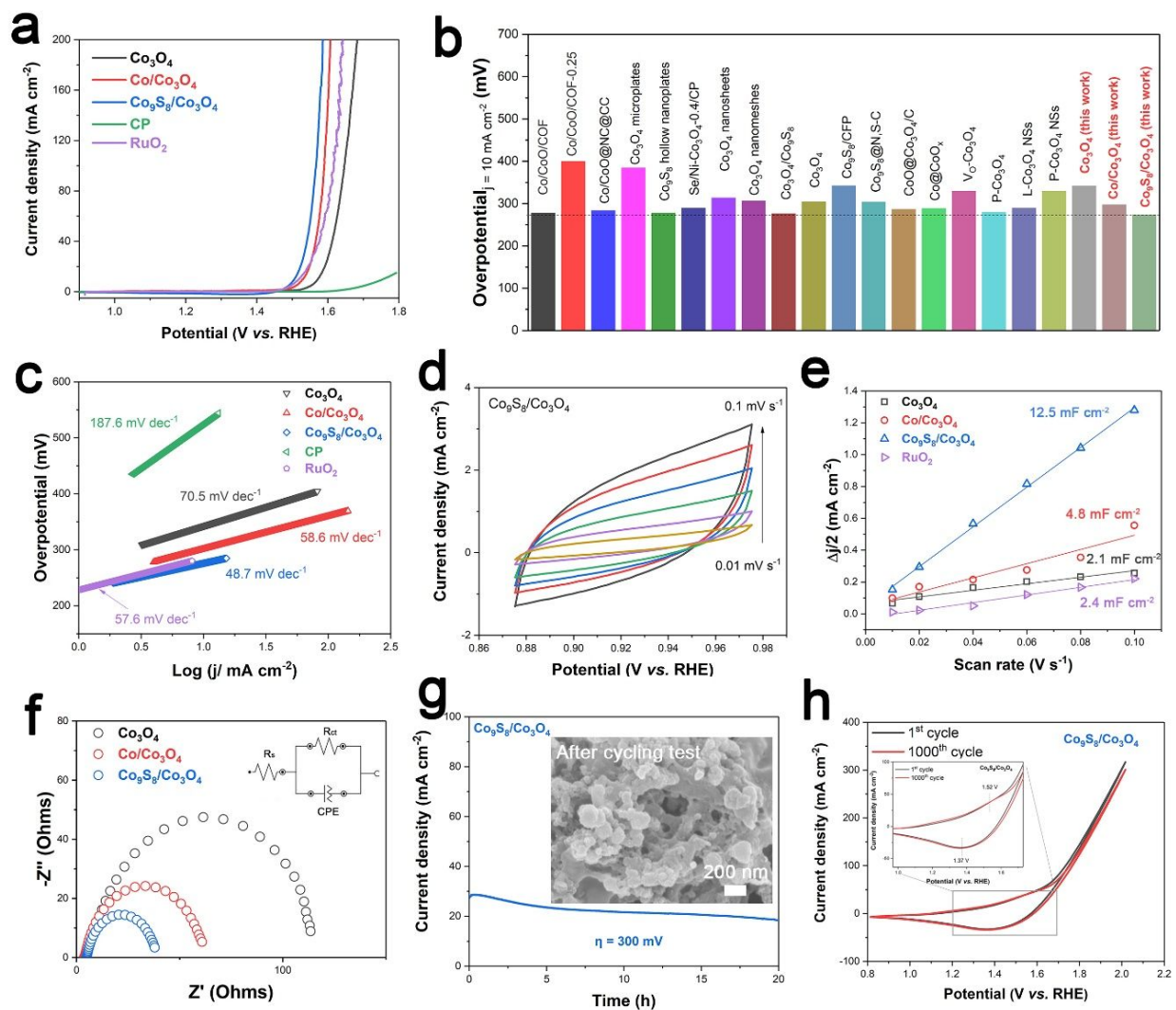
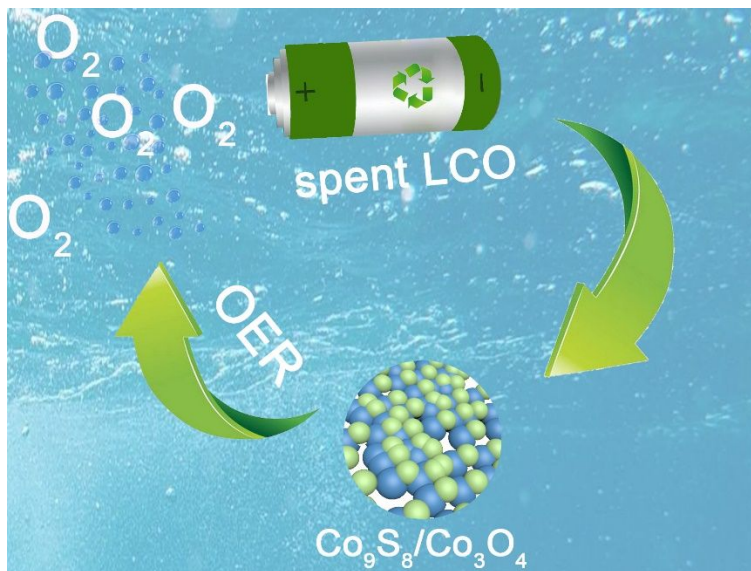


Fig. 4 Electrochemical OER activity of regenerated Co-based catalysts from the spent LCO batteries. a) IR-corrected polarization curves of the Co_3O_4 , $\text{Co}/\text{Co}_3\text{O}_4$, $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$, RuO_2 and carbon paper (CP) in 1 M KOH electrolyte at a scan rate of 2 mV s^{-1} ; b) Comparison result of η_{10} for our catalysts and other Co-based OER catalysts; c) Tafel plots of the catalysts obtained from their corresponding polarization curves; d) CV curves of $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$ at different scan rates from 0.01 to 0.1 V s^{-1} ; e) Current densities versus scan rates measured at a potential value of 0.925 V (vs. RHE) for the obtained catalysts; f) Nyquist plots of the catalysts at an overpotential value of 300 mV for OER; g) The $I-t$ curve of $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$ for OER process at an overpotential

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3 of 300 mV for 20 h (the inset shows the morphology of the sample after long-term cycling test);
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5 h) CV cycling stability test of $\text{Co}_9\text{S}_8/\text{Co}_3\text{O}_4$ at a scan rate of 0.1 V s^{-1} .
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TOC



Waste to treasure: Regeneration of mesoporous Co_9S_8/Co_3O_4 heterostructures for efficient electrochemical oxygen evolution reaction.