

# Diffuse interface modelling of the rheology of immiscible polymer blends

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**U/e** Diffuse interface modelling of the rheology of immiscible polymer blends

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## **Objective**

Predict macroscopic properties of polymer blends, such as the first normal stress difference  $(N_1)$ , based on the information obtained with simulations of morphology development on a microstructural level [1].



$$\boldsymbol{q} = \frac{1}{V} \int (\boldsymbol{n} \cdot \boldsymbol{n} - \frac{1}{3}\boldsymbol{I}) d\Omega .$$
 (1)

$$\frac{N_1 V}{\gamma} = q_{yy} - q_{xx} = \sum (n_{yy,i} - n_{xx,i}) d\Omega_i .$$
<sup>(2)</sup>

The major advantage with respect to the work of Peters [2] is that the model requires *no* additional critical criteria for breakup and coalescence phenomena.

Numerical discretization limits the maximum domainsize ( $\sim$ 50 times the interface thickness  $\xi$ ). Rescaling of the interface is therefore an important issue in diffuse interface modelling.

## **Methods**

The Cahn-Hilliard (CH) equations, based on a diffuse interface approach are used to describe non-uniform systems:

$$\frac{\partial c}{\partial t} + \boldsymbol{v} \cdot \nabla c = \frac{1}{Pe} \nabla^2 \mu , \qquad Pe = \frac{\rho \xi^2 L V}{M \epsilon} , \qquad (3)$$

$$\mu = c^N - c - C^2 \nabla^2 c , \qquad \qquad C = \frac{\xi}{L} , \qquad (4)$$

in which the chemical potential  $\mu$  is the driving force for the topological changes ( $\partial c/\partial t$ ). Besides  $\mu$  and the concentration c the velocity v is unknown in these two equations and has to be calculated using the momentum balance (*eq. 5*) with prescribed simple shear via the boundary conditions:

$$\nabla g = \rho \mu \nabla c + \nabla \cdot (2\eta \boldsymbol{D}) \,. \tag{5}$$

In 2D a stream function  $\psi$ , which is defined by  $v = (\partial \psi / \partial y, -\partial \psi / \partial x)$  can be used to govern balance of mass and by taking the rotation  $\nabla g$  is eliminated. Scaling of this equation then yields:

$$\nabla^4 \psi = \frac{1}{Ca} \frac{1}{C} \nabla \times \mu \nabla c , \qquad \qquad Ca = \frac{\xi \eta V}{\rho \epsilon c_B^2} = \frac{\eta V}{\gamma} , \quad (6)$$

In all subsequent simulations N = 7 in *eq.* 4 to create a more immiscible behaviour between the two components, which corresponds to a higher  $\chi$  parameter.

## /department of mechanical engineering

### Results

The simulations, depicted in figure 1 and 2 are carried out with Pe = 5, C = 0.02 and Ca = 10. Except for the red curves in figure 3 (right), in which the scaling of the interface is tested with C = 0.04 (doubled) and  $Pe_n = (C/C_n)Pe$  ( $\circ$ ),  $Pe_n = (C_n/C)Pe$  ( $\triangleleft$ ) and  $Pe_n = (C_n/C)^2Pe$  (+)



**Figure 1** Break up of one single droplet as a result of prescribed shear on the top and bottom boundary.



**Figure 2** Breakup and coalescence in a multi-droplet domain subjected to a start up flow.



**Figure 3** Left: first normal stress difference  $(N_1)$  scaled with the interfacial tension  $(\gamma)$ . Right: Scaling results of Peclet for thicker interfaces.

In figure 1 the stretching and breakup is observed. In figure 2 more droplets are used to introduce the possibility of coalescence. The red curves in figure 3 (left) show the relaxation of droplets after cessation of shear at various time-steps.

## Conclusions

- The method describes breakup and coalescence without additional decision criteria.
- Scaling of the interface to more realistic domains looks promising, but requires additional work.
- The relation between microscopic and macroscopic parameters can be established.

**References:** 

- [1] TUCKER III, C.L., MOLDENAERS, P.: Microstructural evolution in polymer blends, Ann. Rev. Fluid Mech, 34:177-210,2002
- [2] PETERS, G.W.M., HANSEN, S., MEIJER, H.E.H.: Constitutive modeling of dispersive mixtures, J. of Rheol., 45:3,659-689, 2001