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Stability of Viscoelastic Flows:

Flow Mark Surface Defects in Injection Molding of Polymer Melts

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Introduction

Unstable flows in polymer processing can result in severe limitations on production rates and final product properties. For instance, flow instabilities during injection molding can result in surface defects on polymer parts often referred to as flow marks (figure 1) [1].

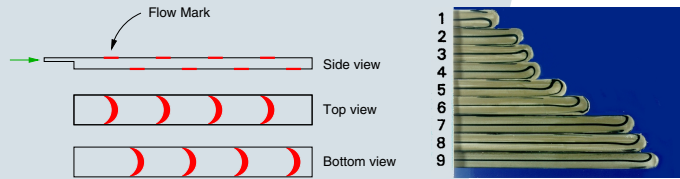


Figure 1: Flow marks in a model injection molding flow. Experiments by M. Bulters and A. Schepens [1].

In an attempt to understand these complex flow phenomena, we have our goals set at:

- Determining the onset of instability
- Isolating rheology dependence

Problem Definition

To analyze these polymer flows, we need to carefully address two important questions:

- 1 What numerical tools can be applied?
- 2 Which rheological model can describe the relevant physics of the polymer melt?

Numerical Tools

In general, a flow is called stable or unstable depending on whether small perturbations imposed on the steady solution decay or grow in time. Thus, the growth rate of a randomly imposed disturbance can be obtained from direct time integration of the governing equations using a finite element technique. Additionally, for simple flows the 1-dimensional generalized eigenvalue problem can be solved for a spectrum of disturbance wavelengths (figure 2).

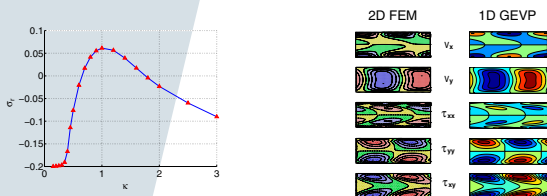


Figure 2: Poiseuille flow of a PTT fluid, maximum growth of a perturbation with spatial wavenumber $\kappa \approx 1$ and $We=5.0$.

Constitutive Models

We consider the widely used exponential Phan-Thien Tanner (PTT) model and the recently proposed eXtended (XPP) Pom-Pom model [3] which is an extension of the original Pom-Pom model as it was introduced by [2].

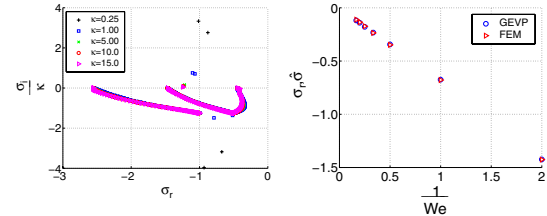


Figure 3: Spectrum (left) and growth rates (right) of Poiseuille flows of an XPP fluid.

Flow Stability

Before moving on to complex flows, we first study the dynamics of planar Poiseuille flows. Figure 2 and figure 3 show the temporal behavior of the PTT and the XPP model for this simple flow. The instability observed with the PTT equations makes this model not suited for stability analyses.

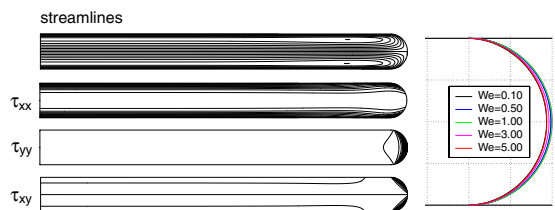


Figure 4: Steady state solution for XPP fluid for $We=5.0$ and shape of the free surface.

Figure 4 shows the steady state solution for the dimensionless Weissenberg number $We=5.0$ which is still computed to be stable for infinitesimal disturbances (figure 5).

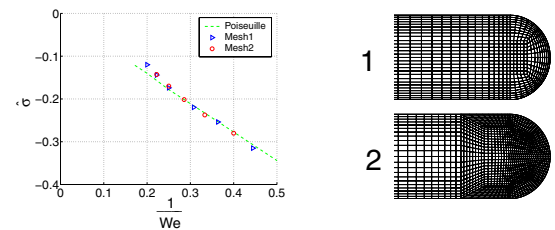


Figure 5: Computed growth rates for an XPP fluid, green line corresponds to growth rates in the upstream channel (Poiseuille flow).

Conclusions

As is demonstrated here, the dynamics of complex polymer flows can efficiently be investigated using transient finite element techniques. Obviously, the choice for the constitutive model plays an important role in the analysis of these flows. In the future, we will extend our analysis towards higher Weissenberg numbers in order to investigate the experimentally observed instability.

References:

- [1] M. BULTERS, A. SCHEPENS: *Proceedings of the 16th Annual Meeting of the Polymer Processing Society, Shanghai (2000)*.
- [2] T.C.B. MCLEISH & R.G. LARSON: *J. RHEOL.* 42(1), 81-110 (1998)
- [3] W.M.H. VERBEETEN et al.: *J. RHEOL.* 45(4), 823-844 (2001)