

# Bio-Based Succinate Production from *Arundo donax* Hydrolysate with the New Natural Succinic Acid-Producing Strain *Basfia succiniciproducens* BPP7

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Abstract Bio-based succinic acid production from lignocellulosic biomass is one of the attractive and prominent alternative technologies to overcome issues associated with the utilization of fossil sources. In this context, it is necessary to find new microorganisms that are able to efficiently ferment this recalcitrant feedstock. The ecological approach developed in this study enabled the isolation of Basfia succiniciproducens BPP7 from a complex rumen ecosystem. This new wild-type strain was able to synthesize up to  $6.06 \pm 0.05$  g/L of succinate (corresponding to  $0.84 \pm 0.017$  g of succinate per gram of consumed glucose + xylose and to  $0.14 \pm 0.001$  g of succinate per gram of glucans + xylans present in the biomass before hydrolysis) from Arundo donax hydrolysate in separate hydrolysis and fermentation (SHF) experiments. Higher titers of succinic acid were obtained through the optimization of growth conditions. The optimal medium composition identified on the smaller scale was then used for 2.5-L batch experiments, which used A. donax hydrolysate and yeast extract as the main C and N sources, respectively. A maximal titer of  $9.4 \pm 0.4$  g/L of succinic acid was obtained after 24 h. The overall results clearly demonstrate the potential of B. succiniciproducens BPP7 for succinate production.

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#### Introduction

Succinic acid (SA) (C<sub>4</sub>H<sub>6</sub>O<sub>4</sub>) is widely used as a precursor for many important chemicals for a broad range of industrial applications, such as the manufacture of solvents, biodegradable plastics, pharmaceuticals, and polymers [1]. Today, SA is primarily produced by chemical processes from the hydrogenation of maleic anhydride to succinic anhydride, followed by hydration to SA [2]. However, due to the high production cost and environmental concerns, there is growing interest in the synthesis of SA based on biological routes, as this dicarboxylic acid is produced as an intermediate of the Krebs cycle or as a product of anaerobic metabolism in microbial fermentations [3]. Many different microorganisms, such as Aspergillus spp., Byssochlamys nivea, Saccharomyces cerevisiae, Anaerobiospirillum succiniciproducens, Actinobacillus succinogenes, Mannheimia succiniciproducens, Basfia succiniciproducens, Fibrobacter succinogenes, Ruminococcus albus, Prevotella ruminicola, Bacteroides amylophilus, and Bacteroides fragilis, isolated from the rumen and other environments, have been assayed and studied for their SA production potential [3, 4]. Additionally, recombinant Escherichia coli strains have been developed to enhance SA production under aerobic and anaerobic conditions [5]. However, bacteria isolated from the rumen are reported as the best SA producers. In fact, high amounts of this C4 dicarboxylic acid are synthesized by CO<sub>2</sub> fixation reactions. The products of these reactions can be converted into propionic acid, providing energy and biosynthetic precursors for the animals [6]. There are different metabolic pathways leading



to SA synthesis. In particular, most bacteria use the phosphoenolpyruvate (PEP) carboxylation reaction (i.e., A. succiniciproducens) [6], whereas others, such as M. succiniciproducens [3, 7], use multiple pathways.

Renewable carbon sources to use in microbial fermentations represent the most prominent eco-technological strategy for bio-based succinate production [8]. One of the most abundant renewable sources is represented by lignocellulosic biomass, including dedicated energy crops such as miscanthus, switchgrass, Arundo donax (giant reed), Populus nigra (poplar), and Eucalyptus camaldulensis (river red gum). These plants can be easily grown in lands not suitable for food crops such as soils that are poor, degraded, or subjected to accelerated erosion [9, 10]. Therefore, due to the abundance and cheapness of raw materials, the use of lignocellulosic biomass hydrolysate is a very attractive and sustainable technology for SA production [1], which may result in processes that are cheaper than petroleum-based processes [6]. Additionally, to satisfy the increasing demand for plastics and to reduce the dependency of plastics on fossil fuels, the development of biopolymers and bio-based plastics from renewable resources is increasing [11].

In the present work, an ecological approach to isolate potential SA-producing bacteria from natural ecosystems was developed. In particular, two SA producer strains, belonging to the *B. succiniciproducens* species, with an attractive substrate utilization spectrum were isolated and tested for their capacity to synthesize succinate from *A. donax*-pretreated lignocellulosic biomass. The optimization of some process parameters, such as agitation and CO<sub>2</sub> sparging, and medium composition were also considered for increasing SA production, together with the implementation of the batch process in 2.5-L fermenters.

#### **Materials and Methods**

## **Isolation and Identification of Bacterial Strains**

Rumens and rumen contents were obtained from 14 freshly slaughtered cattle samples that differed in age, gender, and origin (Table 1). An aliquot (10 g) from each sample was inoculated in 200 mL of minimum salt enrichment medium (MSEM) supplemented with 0.016 g/L lasalocid (Sigma-Aldrich, Milan, Italy) and 0.010 g/L of monensin (Sigma-Aldrich) [3]. The enrichment cultures were incubated at 37 °C in an atmosphere with 5% CO<sub>2</sub> (CO<sub>2</sub> incubator NOVACELL CO 170, Esco CelCulture Incubator, Italy) for 18 h and were serially decimally diluted (up to 10<sup>-7</sup>) in phosphate-buffered saline solution (PBS) and in Luria-Bertani (LB) liquid medium (10 g/L tryptone, 5 g/L yeast extract, 10 g/L NaCl, pH 7.0). One hundred microliters of each PBS dilution was spread on two solid selective isolation

**Table 1** Features of the bovine rumen samples used in this study

Sample	Breed	Age (years)	Breeding location
A	Female buffalo	5	Potenza
В	Female buffalo	4	Matera
C	Steer	6	Potenza
D	Steer	8	Potenza
E	Cow	21	Salerno
F	Cow	11	Potenza
G	Cow	11	Potenza
Н	Cow	8	Salerno
I	Cow	5	Caserta
L	Steer	5	Salerno
M	Cow	9	Salerno
N	Cow	8	Salerno
O	Cow	9	Salerno
P	Cow	16	Salerno

media, SSIM [12] and SSIM1 (20 g/L glucose, 5 g/L peptone, 5 g/L yeast extract, 2 g/L NaCl, 0.4 g/L NaHCO<sub>3</sub>, 0.25 g/L cysteine-HCl, 100 mg/L bacitracin, 1 mg/L lincomycin, 50 mg/L nystatin, 2.5 mg/L bromocresol purple, 12 g/L bacteriological agar, pH 6.5). Concurrently, 100 μL of each LB dilution was spread on Pasteurellaceae selective medium (PSM) [13] containing (per liter) 25 g of brain heart infusion, 50 mL of defibrinated sheep blood, 3.5 mL of β-nicotinamide adenine dinucleotide (β-NAD), 100 mg of bacitracin, 1 mg of lincomycin, 50 mg of nystatin, 100 mg of crystal violet, and 18 g of bacteriological agar. The plates were incubated at 37 °C for 18 h in an atmosphere with 5% CO<sub>2</sub> (CO<sub>2</sub> incubator NOVACELL CO 170).

After incubation, single colonies were randomly isolated on the basis of their colony morphology (i.e., shape, edge, color, elevation, and dimension) by repetitive streaking on the same isolation media and were characterized on the basis of their microscopic morphology (phase-contrast microscopy, shape, and presence of spores) and biochemical features (Gram stains and catalase activity).

Representative isolates of each group were then identified by 16S ribosomal RNA (rRNA) gene sequencing. Total DNA from the bacterial strains was extracted using InstaGene<sup>TM</sup> Matrix (Bio-Rad Laboratories, Hercules, CA, USA) according to the manufacturer's instructions. DNA (approximately 50 ng) was amplified with the primers FD1 (5'-AGA GTT TGA TCC TGG CTC AG-3') and RD1 (5'-AAG GAG GTG ATC CAG CC-3') using a PCR mixture employed as previously described [14]. The PCR conditions were as described by Giacobbe et al. [15]. Amplicons were purified using a QIAquick Gel Extraction kit (Qiagen S.p.A., Milan, Italy), and eluted DNAs were quantified and sequenced as previously reported [16]. Finally, nucleotide sequences were compared to the GenBank nucleotide data library using the



BLAST software at the National Center of Biotechnology Information website (http://www.ncbi.nlm.nih.gov/Blast.cgi).

## **Phylogenetic Analysis**

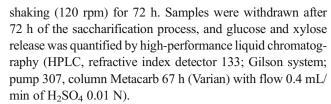
The nearly full-length 16S rRNA sequences of bacterial strains BPP7 and BPP8 and type strains belonging to different genera as described by Kuhnert et al. [13] were used to perform multiple nucleotide alignments using the ClustalW program [17] from MEGA version 4.0 [18]. The nucleotide sequences of the type strains were retrieved from the Ribosomal Database Project (RDP—http://rdPcme.msu.edu/). The phylogenetic tree was inferred using the Neighbor-Joining method with the Maximum Composite Likelihood model in the MEGA4 program, with bootstrap values based on 1000 replications.

#### **PCR-DGGE** Analysis

The total microbial DNA from enriched cultures was extracted using a FastDNA SPIN Kit for Soil (MP Biomedicals, Illkirch Cedex, France) according to the manufacturer's instructions. Primers V3f (5'-CCTACGGGAGGCAGCAG-3') and V3r (5'-ATTACCGCGGCTGCTGG-3') were employed to amplify the V3 hypervariable region of the 16S rRNA gene (200 bp) using a previously described PCR mixture and conditions [19, 20]. The amplicons were analyzed by denaturing gradient gel electrophoresis (DGGE) in a 0.8-mm polyacrylamide gel using a Bio-Rad DCode Universal Mutation System (Bio-Rad, Laboratories, Milan, Italy) as described by Ventorino et al. [21]. After staining the gels for 30 min with SYBR Gold, image analysis of DGGE profiles was performed in Phoretix 1D Pro Gel Analysis Software (TotalLab Ltd., Newcastle, UK). Similarity analysis was performed as described by Marileo et al. [22] with a Bray-Curtis similarity index (5% significance level) and was visualized by nonmetric multidimensional scaling (NMDS) using the software PRIMER-E version 6.1.

#### **SA Production by Pretreated Lignocellulosic Biomass**

A. donax biomass, pretreated according to Garbero et al. [23] and De Bari et al. [24], was utilized as substrate in separate hydrolysis and fermentation (SHF). Hydrolysis was performed by suspending 20 g of pretreated biomass in 100 mL of sodium acetate buffer (0.05 M, pH 5.0) and adding the commercial cellulase mixture Cellic® CTec2, kindly provided by Novozymes (Bagsvaerd, Denmark), with a concentration of 70 FPU/g of pretreated biomass solids. The filter paper cellulase units (FPUs) of the enzyme Cellic® CTec2 were determined according to the standard procedure recommended by the International Union of Pure and Applied Chemistry (IUPAC) [25]. Hydrolysis was performed at 37 °C with



The fermentation step was performed using either the pretreated biomass directly after hydrolysis including solid and liquid fractions (PB) or the clarified hydrolysate including only the liquid fraction that was recovered with a peristaltic pump after 3 h of sedimentation under gravity and drawn (PBS). One hundred milliliters each of PB and PBS was supplemented with MH components (10 g/L polypeptone, 5 g/L yeast extract, 3 g/L K<sub>2</sub>HPO, 2 g/L NaCl, 2 g/L (NH<sub>4</sub>)SO<sub>4</sub>,  $0.2\ g/L\ CaCl_2,\ 0.2\ g/L\ MgCl_2,\ 10\ g/L\ MgCO_3,\ 0.001\ g/L$ Na<sub>2</sub>S, pH 6.5) [3], reaching glucose and xylose concentrations of approximately 12 g/L each. The two obtained media, PBMH and PBSMH, were autoclaved at 120 °C for 15 min and were inoculated with the two selected strains, B. succiniciproducens BPP7 and B. succiniciproducens BPP8, to reach a microbial concentration of approximately 2 × 10<sup>7</sup> cells/mL. Triplicate fermentation experiments were conducted under static anaerobic conditions at 37 °C (Whitley DG250 Anaerobic Workstation, Don Whitley Scientific, Shipley, England). SA production and glucose and xylose consumption were measured by HPLC at 0, 24, 48, and 72 h. SA yield was defined as grams of SA per gram of consumed glucose and xylose (Y<sub>SA/G+X</sub>, g/g) and as grams of SA per gram of total sugars (glucans and xylans) present in the A. donax biomass before hydrolysis (Y<sub>SA/PB</sub>, g/g).

During the SHF process, the growth of the bacterial strains was also determined by spreading tenfold serial dilutions on Brain-Heart Infusion medium (BHI, Oxoid, Milan, Italy). The plates were incubated for 24 h at 37 °C in an atmosphere with 5% CO<sub>2</sub> (CO<sub>2</sub> incubator NOVACELL CO 170).

# Optimization and Scale-up of SA Production in Shake Flasks and 2.5-L Batch Experiments

Optimization of SA production was performed for *B. succiniciproducens* BPP7, which was identified as the best candidate in previous experiments. All cultivations were conducted in 250-mL bottles with 250 mL of medium at 37 °C and shaking at 140 rpm, if necessary, in a rotary shaker incubator (Minitron, Infors, Bottmingen, Switzerland). The bottles were sealed with stainless steel headpiece caps and sterile venting filters to insufflate CO<sub>2</sub>, if necessary, before starting the experiment. Experiments were either conducted on standard MH medium or on a modified medium containing MH salts, supplemented with yeast extract (5, 1, or 0 g/L) and polypeptone (15, 10 or 0 g/L) and in which glucose was replaced by *A. donax* hydrolysate. *A. donax* hydrolysate was diluted to achieve the desired starting concentration of sugars.



Glucose or *A. donax* hydrolysate was autoclaved separately and added to the medium before strain inoculation. The medium pH was adjusted to 6.5.

Cell growth was monitored by removing MgCO<sub>3</sub> from the broth according to Becker et al. [26] to avoid interference of this insoluble compound with biomass quantification. Samples were withdrawn during the course of the experiment to analyze glucose and xylose (if present) consumption and organic acid production. Every experiment was repeated at least three times.

For fermentation experiments, seed cultures were inoculated with the working cell bank and grown in 250-mL bottles as described in the previous section for  $16 \pm 1$  h on MH medium with glucose as a C source and yeast extract as a complex nitrogen source. The main cultures were grown on a Biostat CT (Sartorius Stedim; Melsungen, Germany) filled with a final volume of 2.5 L of broth composed by MH components, yeast extract as a complex nitrogen source, and *A. donax* hydrolysate as carbon source (starting glucose concentration of 4.3 or 8.0 g/L and starting xylose concentration of 2.5 or 4.7 g/L for experiment 1 and experiment 2, respectively). All experiments were conducted at 37 °C with  $CO_2$  sparging at 0.5 vvm and an agitation speed set to 100 rpm. A constant pH of 6.5 was maintained via automated addition of NH<sub>4</sub>OH (Sigma-Aldrich).

Broth samples were collected every 2 h during cultivation to follow biomass formation (when possible), substrate consumption, and product formation. The supernatants obtained after centrifugation at  $5000\times g$  were ultrafiltered on 3-kDa Centricon devices (Millipore, Bedford, MA, USA), and the flowthrough was analyzed by HPLC in an UltiMate 3000 on an Alltech IOA-2000 column (500 mm  $\times$  6.5 mm ID) at 40 °C with 0.1% v/v phosphoric acid in water as the mobile phase at a flow rate of 0.6 mL/min. Detection was performed via UV absorbance at 200 nm and refraction index (Shodex RI-101 detector, max auto step 5.1 s, temperature 32 °C, rise time 1 s, polarity plus, record range 512 µRIU, integrator range 500 µRIU/UV).

#### **Statistical Analyses**

One-way ANOVA followed by Duncan's post hoc test for pairwise comparison of means (at  $p \le 0.05$ ) was used to assess the difference in the SA production on different fermentation media. Statistical analyses were performed using the SPSS 21.0 statistical software package (SPSS Inc., Cary, NC, USA) [27].

#### **Nucleotide Sequence Accession Numbers**

The 16S rRNA gene sequences obtained from the bacterial strains were deposited in the GenBank database under accession numbers KT362365 and KT362366 for the strains BPP7 and BPP8, respectively, and from KX156160 to KX156256 for the other strains.

#### **Results and Discussion**

# Microbial Diversity and Isolation of Putative SA-Producing Bacteria

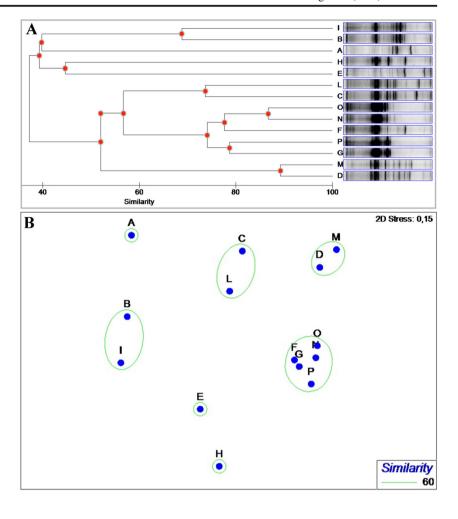
Bacterial diversity of the enriched cultures was evaluated using a culture-independent approach with PCR-DGGE to detect changes of complex bacterial communities in the environment based on different profiles obtained by base-pair sequences of amplicons with the same length [28]. This methodology demonstrated a high biodiversity among samples, with similarity levels from 35 to 90% (Fig. 1a). The DGGE profiles obtained were used to evaluate the levels of similarity of the bacterial community between the different rumen samples by cluster analysis. As shown in Fig. 1b, the samples could be grouped into seven major clusters. One group included five rumen samples (F, G, N, O, and P), whereas the other six groups consisted of two (cluster 2: D and M; cluster 3: C and L; cluster 4: I and B) or one (cluster 5: A; cluster 6: E; cluster 7: H) rumen sample (Fig. 1b). Interestingly, the diversity of bacterial populations investigated using this cultureindependent approach highlighted that it did not seem to be influenced by the features of the samples, such as breed, age, and geographical origin, described in Table 1. In fact, the cluster 1 grouped samples originated from cows aged from 8 to 16 years that were bred in Potenza (Basilicata region, Italy) and Salerno (Campania region, Italy), and the cluster 2 grouped samples originated from cows and steers bred in Potenza and Salerno. Similar results were also shown for samples grouped in the other clusters.

The bacterial diversity of the enriched cultures was also evaluated using a culture-dependent approach to isolate and select SA-producing microorganisms. The selective culturedependent approach used in this work enabled for the isolation of facultative anaerobic and/or microaerophilic bacteria from rumen samples characterized by the presence of fermentative microorganisms and, in particular, potential SA-producing microbes. In fact, the two ionoporic antibiotics, lasalocid and monensin, that were added to the media inhibited acetic acid-producing and hydrogen-producing microorganisms, usually present in the rumen, and favored the growth of SAand propionic acid-producing bacteria [29]. A total of 364 potential SA-producing bacteria were isolated and grouped on the basis of their colony and microscopic morphologies and on their biochemical features (data not shown). Among these bacteria, 99 representative strains were selected and identified by 16S rRNA gene sequencing. The molecular identification resulted in bacterial isolates with great biodiversity, as 21 genera and 37 different species were found (Fig. 2).

Enterobacteriales was the most represented order (48.5%), consisting of the genera *Proteus* spp. (33.33%), *Providencia* spp. (5.05%), *Raoultella* spp. (4.04%), *Pantoea* spp. (1.01%), *Citrobacter* spp. (1.01%), *Klebsiella* spp. (1.01%), *Serratia* 



Fig. 1 DGGE profiles and cluster analysis (a) and non-metric multidimensional scaling analysis (NMDS) of DGGE profiles (b) of the bacterial communities in the enriched cultures



spp. (1.01%), Hafnia spp. (1.01%), and Obesumbacterium spp. (1.01%). Bacteria belonging to the genera *Proteus* spp., Raoultella spp., Citrobacter spp., and Klebsiella spp. were recovered in the ruminal fluid of dairy cattle, rumen samples, and bovine fecal material [30-32]; their occurrence in ruminants could be expected because some of these genera, such as Pantoea, Raoultella, and Citrobacter, are reported to be cellulase-producing bacteria [10, 33]. Moreover, according to Mao et al. [34], in addition to Proteobacteria, Firmicutes is a predominant phylum found in rumen samples of dairy cattle. In fact, in this study, Bacillales and Lactobacillales, covering 28.3 and 18.2% of bacterial biodiversity, respectively, were the other orders recovered at high incidence, although their occurrence depended on cattle sample types. Lactobacillales, strongly dominated by Enterococcus spp. (8.08%), followed by Weissella (5.05%), Lactococcus (3.03%), *Lactobacillus* (1.01%), and *Streptococcus* (1.01%), were mainly isolated from samples L and P. By contrast, Bacillales were isolated from all samples except for the L and M samples. Bacteria belonging to the genus Bacillus covered 23.23% of the isolated strains (Fig. 2). This ubiquitous genus includes different cellulolytic bacteria exhibiting interesting enzymatic activities for the hydrolysis of lignocellulosic biomass carbohydrates into fermentable sugars for a wide range of industrial applications [35–37].

Finally, to a lesser extent, bacteria belonging to *Acinetobacter* spp. (2.0%), *Basfia* spp. (2.0%), and *Comamonas* spp. (1.0%) were also recovered (Fig. 2). Among all isolates, the two new strains, *B. succiniciproducens* BPP7 and *B. succiniciproducens* BPP8, were the most promising microorganisms, as the bacteria belonging to this species have been reported to be efficient producers of SA [13]. Therefore, to confirm the molecular identification of these bacterial strains, a phylogenetic tree was constructed. The results of the Neighbor-Joining analysis of the 16S rRNA sequences of the bacterial strains are shown in the dendrogram depicted in Fig. 3. The closest relative species was *B. succiniciproducens*, demonstrating that strains BPP7 and BPP8 could be ascribed to this species.

#### **SA Production and Optimization**

The preliminary fermentation screening of 20 representative strains in 100 mL of MH-rich medium supplemented with 20 g/L glucose was performed to select the best SA-producing bacteria. Among all tested strains, chosen on the basis of molecular identification and incidence percentage,



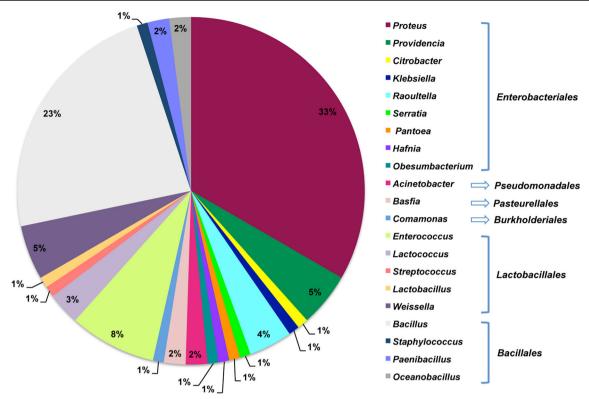


Fig. 2 Percentage compositions of different genera of bacterial strains isolated from enriched cultures on the basis of 16S rRNA gene sequence similarity

only *B. succiniciproducens* BPP7 and *B. succiniciproducens* BPP8 were able to secrete large amounts of succinate (data not shown).

On the basis of the preliminary results, these two strains were selected and evaluated for their capacity to synthesize succinate from pretreated lignocellulosic biomass of *A. donax* in SHF using either the pretreated biomass directly after hydrolysis (PB) or the liquid fraction (PBS). Due to its high carbohydrate contents and capacity to grow in marginal and contaminated lands not suitable for food crops [38], the lignocellulosic biomass of *A. donax* is an interesting substrate for bioconversion to SA. Moreover, although different waste and lignocellulosic materials, such as corncobs, corn stover, rapeseed, rice, wheat straw, switchgrass, bagasse, and oak wood [1, 39], have been employed to produce bio-based chemicals, the use of *A. donax* hydrolysate as a substrate for SA production was first reported only recently [12].

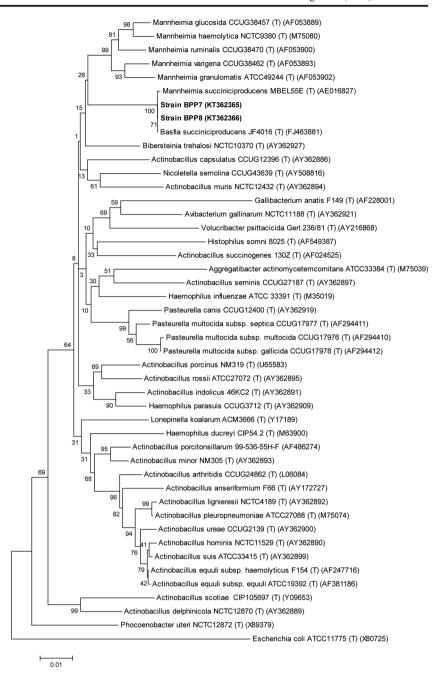
In SHF experiments, the two new bacterial strains were able to synthesize high levels of succinate in all tested conditions. In particular, the concentration of SA recovered from strain *B. succiniciproducens* BPP7 was notable after 24 h (glucose and xylose consumption of approximately 45%), increasing up to 4.38  $\pm$  0.09 g/L (Y<sub>SA/G+X</sub> of 0.39  $\pm$  0.010 g/g and Y<sub>SA/PB</sub> of 0.10  $\pm$  0.002 g/g) and 6.06  $\pm$  0.05 g/L (Y<sub>SA/G+X</sub> of 0.84  $\pm$  0.017 g/g and Y<sub>SA/PB</sub> of 0.14  $\pm$  0.001 g/g) after 48 h using PBMH and PBSMH, respectively (Table 2). However,

in PBMH, there were no significant differences (p > 0.05) among the three sampling times (24, 48, and 72 h), whereas in the PBSMH substrate, the SA production significantly decreased after 72 h (Table 2). These results emphasized that the use of *A. donax* hydrolysate recovered by sedimentation under the gravity method promoted the fermentation activity of the strain *B. succiniciproducens* BPP7, showing the highest succinate production and yield. This result could be due to the presence of specific toxic compounds (e.g., furfural, HMF, phydroxybenzoic aldehyde, and vaniline) in solid components of the pretreated biomass hydrolysate used in the PBMH medium. These compounds are known to have an inhibitory effect on microbial metabolism, limiting the efficiency of conversion of fermentable sugars in biochemicals and biofuels [40].

Similar results were obtained using the strain *B. succiniciproducens* BPP8. In fact, after 24 h, most of the glucose and xylose consumption (approximately 50%) and notable synthesis of succinate were recorded (Table 2). In PBMH and PBSMH conditions, after 48 h of fermentation, the SA production significantly increased up to  $4.03 \pm 0.07$  g/L (Y<sub>SA/G+X</sub> of  $0.34 \pm 0.009$  g/g and Y<sub>SA/PB</sub> of  $0.09 \pm 0.002$  g/g) and  $5.37 \pm 0.06$  g/L (Y<sub>SA/G+X</sub> of  $0.84 \pm 0.020$  g/g and Y<sub>SA/PB</sub> of  $0.12 \pm 0.001$  g/g), respectively (Table 2), emphasizing that this strain also exhibited the highest succinate amount and yield in the PBSMH condition. Nevertheless, in both tested



Fig. 3 Neighbor-Joining tree based on the comparison of 16S rRNA gene sequences showing the phylogenetic relationships among strains BBP7 and BPP8 isolated in this study and type strains. Bootstrap values (expressed as percentages of 1000 replications) are given at the nodes. The sequence accession numbers used for the phylogenetic analysis are shown in parentheses following the species names. Strains marked with "(T)" represent type strains. The scale bar estimates the number of substitutions per site



conditions, either the succinate concentration decreased or no significant differences were observed after 72 h.

However, the SA production capacity of strain *B. succiniciproducens* BPP7 was higher than that of *B. succiniciproducens* BPP8 on both PBSMH (+12.85%) and PBMH (+8.68%) after 48 h. Moreover, considering the highest SA synthesis of the strain *B. succiniciproducens* BPP7, the mass balance from 1 kg of pretreated *A. donax* biomass (containing 0.1 kg of glucans and xylans) was 0.014 kg of SA. Therefore, on the basis of these results, additional experiments in larger bottles were performed to further optimize the production of SA from *B. succiniciproducens* 

BPP7. The effects of agitation and CO<sub>2</sub> sparging on biomass and SA production to identify the best operating conditions were initially investigated. These preliminary assays were performed on MH-rich medium containing glucose as a C source to avoid interference due to other factors linked to the presence of a complex substrate such as *A. donax* hydrolysate. As shown in Table 3, after 24 h of growth, more SA was produced in the agitated cultures and a further slight improvement was obtained by creating an anaerobic environment with CO<sub>2</sub> sparging, resulting in 0.75 g of SA per gram of glucose and a final titer of approximately 8 g/L of the target molecule. In all setups, glucose was never exhausted from the medium



Succinic acid (SA) concentrations (gL) and yields defined as grams of SA per gram of consumed glucose and xylose (Y<sub>SA/G+X</sub>, g/g) and as grams of SA per gram of glucans and xylans present in the A. donax biomass before hydrolysis ( $Y_{SAPB}$ , g/g) of the strains B. succiniciproducens BPP7 and B. succiniciproducens BPP8 from SHF in anaerobic conditions during 72 h of fermentation at 37 °C static conditions

Time (h)	Time (h) Basfia succiniciproducens BPP7	iproducens BPP7	7				Basfia succini	Basfia succiniciproducens BPP8	86			
	PBMH			PBSMH			PBMH			PBSMH		
	SA (g/L)	$SA(gL) \qquad Y_{SAG+X}(g/g)  Y_{SAPB}(g/g)  SA(g/L) \qquad Y_{SAG+X}(g/g)  Y_{SAPB}(g/g)  SA(g/L) \qquad Y_{SAG+X}(g/g)  Y_{SAG+X}(g$	$Y_{SA/PB}$ (g/g)	SA (g/L)	$Y_{\rm SA/G+X}~(g/g)$	$Y_{\rm SA/PB}~(g/g)$	SA (g/L)	$Y_{\rm SA/G+X}~(g/g)$	$Y_{SA/PB}$ (g/g)	SA (g/L)	$Y_{SA/G+X}\ (g/g)$	$Y_{SA/PB}$ (g/g)
0 24 48 72	$0.00 \pm 0.00^{A}$ $4.21 \pm 0.10^{C}$ $4.38 \pm 0.09^{D}$ $4.29 \pm 0.02^{CD}$	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	$0.00 \pm 0.000^{A}$ $0.09 \pm 0.002^{B}$ $0.10 \pm 0.002^{C}$ $0.10 \pm 0.000^{C}$	$0.00 \pm 0.00^{A}$ $3.87 \pm 0.04^{B}$ $6.06 \pm 0.05^{F}$ $5.91 \pm 0.07^{E}$	$0.00 \pm 0.000^{A}$ $0.45 \pm 0.010^{D}$ $0.84 \pm 0.017^{F}$ $0.81 \pm 0.034^{E}$	$0.00 \pm 0.000^{A}$ $0.09 \pm 0.001^{B}$ $0.14 \pm 0.001^{E}$ $0.13 \pm 0.002^{D}$	$0.00 \pm 0.00^{A}$ $3.93 \pm 0.08^{C}$ $4.03 \pm 0.07^{D}$ $3.77 \pm 0.05^{B}$	$0.00 \pm 0.000^{A}$ $0.32 \pm 0.010^{B}$ $0.34 \pm 0.009^{B}$ $0.29 \pm 0.007^{B}$	$0.00 \pm 0.000^{A}$ $0.09 \pm 0.002^{C}$ $0.09 \pm 0.002^{C}$ $0.08 \pm 0.001^{B}$	$0.00 \pm 0.00^{A}$ $4.30 \pm 0.04^{E}$ $5.37 \pm 0.06^{F}$ $5.45 \pm 0.08^{F}$	$0.00 \pm 0.000^{A}$ $0.65 \pm 0.011^{C}$ $0.84 \pm 0.020^{D}$ $0.96 \pm 0.089^{E}$	$0.00 \pm 0.000^{A}$ $0.10 \pm 0.001^{D}$ $0.12 \pm 0.001^{E}$ $0.12 \pm 0.002^{E}$

he values represent the means  $\pm$  SD of three replicates of independent experiments. Different letters after the values indicate significant differences ( $p \le 0.05$ ) among the succinate concentration (gL) or PBMH A. donax biomass hydrolysate supplemented with MH components, PBSMH liquid components of A. donax biomass hydrolysate recovered after sedimentation and supplemented with MH Y<sub>SA/G+X</sub> (g/g) or Y<sub>SA/PB</sub> (g/g) values in each strain

components

Production of biomass, succinic acid (SA), and acetic acid of strain B. succiniciproducens BPP7 on MH standard medium containing 20 g/L glucose in batch cultivations conducted in bottles for 24 h

Conditions	SA (g/L)	OD <sub>600</sub>	Acetic acid (g/L)	Y <sub>SA/G</sub> (g/g)
S <sub>24h</sub>	$4.40 \pm 0.87$	$3.88 \pm 0.12$	$2.91 \pm 0.16$	$0.59 \pm 0.06$
$S + CO_{2 24h}$	$6.37 \pm 0.62$	$3.67 \pm 0.12$	$3.17 \pm 0.11$	$1.11\pm0.12$
$A_{24h}$	$7.92\pm1.18$	$6.80\pm1.19$	$3.32\pm1.69$	$0.67\pm0.05$
$A + CO_{2\ 24h}$	$8.21 \pm 0.35$	$6.35\pm0.52$	$4.59 \pm 0.24$	$0.75\pm0.10$
$S + CO_{2 24h}$ $A_{24h}$	$6.37 \pm 0.62$ $7.92 \pm 1.18$	$3.67 \pm 0.12$ $6.80 \pm 1.19$	$3.17 \pm 0.11$ $3.32 \pm 1.69$	$1.11 \pm 0.12$ $0.67 \pm 0.02$

S static, A agitation, CO<sub>2</sub> initial sparging with CO<sub>2</sub> to create an anaerobic environment,  $Y_{SA/G}$  grams of succinate produced per gram of consumed

during the 24 h of growth, and the major by-product was acetate (Table 3). The results obtained in this work highlight that the selected wild-type strain B. succiniciproducens BPP7 could be considered a natural high SA producer due to its SA yield (0.75 g/g), as it showed similar or higher SA levels compared with those produced by other wild-type B. succiniciproducens strains. In fact, the new natural strain BPP7 synthesized up to 8 g/L, with a yield of 0.75 g/g of SA, starting from the synthetic substrate MH containing 20 g/L of glucose, whereas the capacities of different wild-type strains of B. succiniciproducens that produced approximately 5 g/L from a synthetic substrate (BHI) with 20 g/L of glucose were described by Kuhnert et al. [13]. Similarly, Becker et al. [26] reported the natural capacity of the wild-type strain B. succiniciproducens DD1 to synthesize SA with a metabolic yield of 0.49 g/g, starting from 45 g/L of glucose. However, the biotechnological performance of B. succiniciproducens BPP7 is also comparable to that obtained in other studies using genetically modified strains of B. succiniciproducens in synthetic media with glucose as the carbon source. Becker et al. [26] significantly improved Y<sub>SA/G</sub> up to 0.71 g/g by engineering B. succiniciproducens DD1 by the double deletion of pyruvate formate lyase (pflD) and lactate dehydrogenase (ldhA). Production of succinate by the mutant LU15224 pJFF224 (icl ms Y.m.), obtained from B. succiniciproducens DD1 engineered by the double knockout of  $\Delta ldh$  and  $\Delta pflD$ . which over-expresses the plasmid pJFF224 (icl ms Y.m.) and contains the glyoxylate shunt operon genes of Yersinia molaretii, resulted in a yield of 0.87 g/g [41].

A second set of experiments was performed on MH medium supplemented with A. donax hydrolysate directly recovered after sedimentation (PBSMH) with the aim to simplify medium composition. Soy peptone was revealed to be unnecessary whereas the addition of yeast extract to the hydrolysate resulted in the highest final titer of SA, approximately 6 g/L after 24 h (Table 4). This corresponded to a Y<sub>SA/G+X</sub> of  $1.08 \pm 0.27$  g/g, almost threefold higher compared to that obtained in the control experiment, and to a Y<sub>SA/PB</sub> of  $0.64 \pm 0.06$  g/g. In addition, a 100% increased productivity



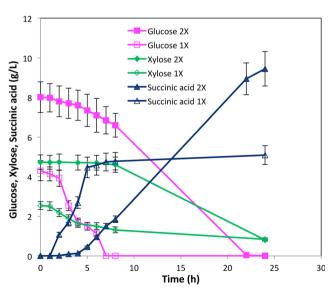
Table 4 Production of succinic acid (SA) of the strain *B. succiniciproducens* BPP7 in 250-mL bottle experiments using *A. donax* hydrolysate in the PBSMH condition. Different concentrations and ratios of soy peptone and yeast extract were evaluated

Soy peptone (g/L)	Yeast extract (g/L)	SA (g/L)	Acetic acid (g/L)	Ethanol (g/L)	$Y_{SA/G+X}$ $(g/g)$	Y <sub>SA/PB</sub> (g/g)
10	5	$4.20 \pm 0.73$	$3.10 \pm 0.20$	$1.87 \pm 0.43$	$0.39 \pm 0.09$	$0.23 \pm 0.03$
15	1	$5.47 \pm 0.30$	$1.86 \pm 0.40$	$0.89 \pm 0.12$	$0.66 \pm 0.04$	$0.06\pm0.00$
0	5	$6.00\pm0.89$	$1.38 \pm 0.28$	$0.19 \pm 0.02$	$1.08\pm0.27$	$0.64 \pm 0.06$
0	0	$2.60 \pm 0.80$	$1.45\pm0.35$	$1.25\pm0.10$	$0.22 \pm 0.10$	$0.14 \pm 0.04$

The cultivations were performed in batch conditions for 24 h at 37  $^{\circ}$ C with initial sparging of CO<sub>2</sub> and agitation.  $Y_{SA/G+X}$  indicates grams of succinic acid produced per gram of glucose and xylose consumed.  $Y_{SA/PB}$  indicates grams of succinic acid on grams of glucans and xylan present in *A.donax* before hydrolysis

(Y<sub>SA/L·h</sub>) was obtained compared with values observed in 100-mL SHF experiments on *A. donax* hydrolysate recovered after sedimentation. Moreover, elimination of soy peptone also decreased the amount of ethanol produced by almost tenfold indicating a redistribution of carbon fluxes. Therefore, even though the complex nitrogen sources were reduced (i.e., no polypeptone), improved process characteristics were successfully demonstrated. However, acetic acid remained the major by-product in all media tested.

On the basis of these results, *B. succiniciproducens* BPP7 was finally analyzed in 2.5-L batch experiments in the optimized cultivation conditions identified in previous bottle experiments (anaerobic conditions, only yeast extract as a complex nitrogen source). *A. donax* hydrolysate was diluted, and two experiments with increasing initial concentrations of glucose and xylose were performed. The experiments lasted 24 h,



**Fig. 4** *B. succiniciproducens* BPP7 grown in batch fermentation experiments with *A. donax* hydrolysate in PBSMH containing yeast extract as a complex nitrogen source with different initial concentrations of glucose and xylose. Experiments were conducted at 37 °C with continuous sparging of CO<sub>2</sub> at 0.5 vvm. Starting concentrations of glucose in the medium are denoted as 2X for 8.0 g/L and 1X for 4.3 g/L; starting concentrations of xylose in the medium are denoted as 2X for 4.7 g/L and 1X for 2.5 g/L

and the final concentrations of SA were measured at approximately 5 and 9 g/L, respectively (Fig. 4). The yields of SA and acetic acid (the major organic acid by-products) on total consumed sugars (glucose and xylose) were consistent in the two batches and corresponded to  $0.84 \pm 0.01$  and  $0.30 \pm 0.04$  g/g, respectively (Fig. 4). Therefore, process scalability was assessed, and batch experiments with higher initial sugar concentrations in the A. donax hydrolysate demonstrated the reproducibility of the Y<sub>SA/G+X</sub>. The yield of succinic acid on the total polysaccharides (glucans and xylans) present in A. donax before hydrolysis was equal to  $0.71 \pm 0.02$  g/g, indicating a slight improvement compared to that obtained in bottle experiments in similar conditions. In addition, using the optimized cultivation conditions in 2.5-L batch experiments, the mass balance from 1 kg of pretreated A. donax biomass (containing 0.1 kg of glucans and xylans) was 0.072 kg of SA.

Overall, these results highlight the high biotechnological potential of the natural SA-producing selected wild-type strain B. succiniciproducens BPP7 to produce second-generation biochemicals. B. succiniciproducens is relatively unexplored if it is to be considered for its potential to synthesize SA from lignocellulosic biomass and, in particular, from A. donax hydrolysate. As reported above, few examples of wild-type and engineered B. succiniciproducens-producing high titers of SA are present in the literature, and most are based on fermentation processes that exploit refined carbon sources (i.e., purified sugars) [42]. Pateraki et al. [43] in fermentation experiments using a mixture of C5 and C6 sugars obtained a succinic acid yield (referring to grams of succinic acid produced per gram of total sugars consumed) up to 0.76 and 0.69 g/g for B. succiniciproducens DSM 22022 and A. succinogenes DSM 22257, respectively. Recently, the ability to synthetize succinic acid from spent sulfite liquor (aqueous waste stream containing solubilized lignin and sugars resulting from hemicellulose degradation) of the strains B. succiniciproducens DSM 22022 (yield from 0.45 to 0.58 g per gram of consumed sugars) was reported [44]. However, the challenge is to develop strategies that enable the exploitation of sugars contained in renewable resources that are not competing with foodborne sources. Only recently, the capacity of the wild-type strain B. succiniciproducens DSM 22022 to synthesize succinate



from corn stover hydrolysate was first investigated [45]. However, Salvachúa et al. [45] reported that the maximum SA yield was 0.69 g/g lignocellulosic hydrolysate at an initial sugar concentration of 60 g/L. This value is lower than that recovered in this study in the different fermentation conditions using *A. donax* hydrolysate at an initial sugar concentration from 12 to 24 g/L (Y<sub>SA/G+X</sub> of 0.84 g/g).

#### **Conclusions**

In conclusion, the ecological strategy employed in this study enabled the isolation of new bacterial strains that are able to synthesize SA from renewable lignocellulosic biomass. The natural SA-producing selected wild-type strain *B. succiniciproducens* BPP7 demonstrated interesting biotechnological applications, as it efficiently fermented *A. donax* hydrolysate, thereby producing succinate. The yield obtained in small-scale shake flask experiments was confirmed in 2.5-L bioreactors on a simplified medium containing *A. donax* supplemented with yeast extract. Although process development is still necessary to reach industrially appealing titers, the results obtained thus far are promising.

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