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# Al<sub>2</sub>O<sub>3</sub> nanofibers prepared from aluminum Di(*sec*-butoxide)acetoacetic ester chelate exhibits high surface area and acidity

M.A. Rodriguez-Olguin<sup>a</sup>, H. Atia<sup>b</sup>, M. Bosco<sup>c,d</sup>, A. Aguirre<sup>c</sup>, R. Eckelt<sup>b</sup>, E.D. Asuquo<sup>e</sup>, M. Vandichel<sup>f,\*</sup>, J.G.E. Gardeniers<sup>a,\*</sup>, A. Susarrey-Arce<sup>a,\*</sup>

<sup>a</sup> Mesoscale Chemical Systems, MESA+ Institute, University of Twente, PO. Box 217, 7500AE Enschede, the Netherlands

<sup>b</sup> Leibniz Institute for Catalysis, Albert-Einstein-Straße 29a, D-18059 Rostock, Germany

<sup>c</sup> Instituto de Desarrollo Tecnológico para la Industria Química (INTEC), Universidad Nacional del Litoral, CONICET, Güemes 3450, S3000GLN Santa Fe, Argentina

<sup>d</sup> Facultad de Ingeniería Química, Universidad Nacional del Litoral (UNL), Santiago del Estero 2829, Santa Fe 3000, Argentina

<sup>e</sup> National Graphene Institute, Department of Materials, University of Manchester, Oxford Road, Manchester M13 9PL, United Kingdom

<sup>f</sup>Department of Chemical Sciences and Bernal Institute, University of Limerick, Limerick V94 T9PX, Republic of Ireland

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### ABSTRACT

Alumina (Al<sub>2</sub>O<sub>3</sub>) is a widely used material for catalysis in the chemical industry. Besides a high specific surface area, acid sites on Al<sub>2</sub>O<sub>3</sub> play a crucial role in the chemical transformation of adsorbed molecules, which ultimately react and desorb from the catalyst. This study introduces a synthetic method based on electrospinning to produce Al<sub>2</sub>O<sub>3</sub> nanofibers (ANFs) with acidity and porosity tuned using different aluminum precursor formulations. After electrospinning and heat treatment, the nanofibers form a nonwoven network with macropores ( $\sim 4 \mu m$ ). Nanofibers produced from aluminum di(sec-butoxide) acetoacetic ester chelate (ASB) show the highest total acidity of ca. 0.70  $\mu$ mol/m<sup>2</sup> determined with temperature-programmed desorption of ammonia (NH<sub>3</sub>-TPD) and BET. The nature of the acid site in ASB ANFs is studied in detail with infrared (IR) spectroscopy. Pyridine is used as a molecular probe for the identification of acid sites in ASB. Pyridine showed the presence of Lewis acid sites prominently. Density-functional theory (DFT) is conducted to understand the desorption kinetics of the adsorbed chemical species, such as ammonia (NH<sub>3</sub>) on crystalline  $\gamma$ -Al<sub>2</sub>O<sub>3</sub>. For our analysis, we focused on a mobile approach for chemisorbed and physisorbed NH<sub>3</sub>. The computational results are compared with NH<sub>3</sub>-TPD experiments, ultimately utilized to estimate the desorption energy and kinetic desorption parameters. The experiments are found to pair up with our simulation results. We predict that these non-woven structures will find application as a dispersion medium of metallic particles in catalysis.

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### 1. Introduction

Al<sub>2</sub>O<sub>3</sub> is one of the most important acid catalysts applied in biomass conversion to produce chemicals and fuels [1–6]. The material also functions as a dispersion medium (i.e., support) for alkali metals, halogens, noble metals, and metal oxides in the petroleum and automotive sector [7–13]. Various polymorphs  $\alpha$ -,  $\gamma$ -,  $\eta$ -,  $\theta$ -,  $\delta$ -,  $\kappa$ -, and  $\chi$ - of Al<sub>2</sub>O<sub>3</sub> can be found in literature [14,15]. This wide range of Al<sub>2</sub>O<sub>3</sub> has unique properties, such as acidity, high specific surface area, and excellent chemical and thermal stability [4,13,16–20]. Among these properties, a key characteristic in Al<sub>2</sub>O<sub>3</sub> is the acid site [21,22,23]. Favorable combinations of acid

\* Corresponding authors.

sites, such as Brønsted acid sites (BAS) and Lewis acid sites (LAS), can be achieved by changing the Al precursor or the addition of other additives during  $Al_2O_3$  synthesis [24–27]. Another key parameter is the pore size distribution.  $Al_2O_3$  can contain different types of porosity, where the micropores, with a pore width distribution lower than 2 nm, contain the active sites for (selective) reaction, and mesopores, with a pore width distribution in the range of 2 to 50 nm, are the diffusion pathways [4,28,29]. Ultramicropores and supramicropores with a pore size between 0.7 and 2 nm,[30] are not discussed here but are known to contribute to the total surface area.

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Synthetic approaches for the production of Al<sub>2</sub>O<sub>3</sub> and its properties have been extensively studied over the years [4,31–55]. Typical methods to structure Al<sub>2</sub>O<sub>3</sub> are extrusion[13], anodization[56], injection molding,[57] and 3D-printing [57,58]. Current developments are focused on geometrical optimization to control reaction

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*E-mail addresses:* matthias.vandichel@ul.ie (M. Vandichel), j.g.e.gardeniers@utwente.nl (J.G.E. Gardeniers), a.susarreyarce@utwente.nl (A. Susarrey-Arce).

rates via mass transfer and diffusivity but often do not pay much attention to the chemical properties of structured Al<sub>2</sub>O<sub>3</sub>. A way to introduce hierarchy in Al<sub>2</sub>O<sub>3</sub> catalysts is by shaping the material in the form of a non-woven nanofiber network. The general idea is that the fiber network will generate macropores that facilitate reactant and product diffusion, whereas the intrinsic porosity in ANFs will provide efficient surface area for reaction kinetics [59,60]. Many applications for non-woven nanofibers have already been promoted, e.g., in environmental science, energy storage, and energy conversion [28,61–65]. However, applications of ANFs in catalysis are still limited (**Table S1** and **Table S2**), possibly due to the difficulty of obtaining ANFs with both high surface area and acidity comparable to known commercial catalysts.

A convenient method for the production of non-woven nanofiber networks is electrospinning [28,64,66–83]. A drawback of this method, compared to many other 3D printing methods, is that electrospinning generally lacks the control to make ordered spaces between intertwining nanofibers. Advancements in the field of electrospinning have demonstrated the possibility of aligning nanofibers (e.g., melting electrospinning),[86] but the method is still limited to polymers and biomaterials [84]. Nevertheless, the electrospinning technique provides excellent precursor versatility, which can be tuned to obtain various functionalities (Table S1). For example, it has been recognized that the role of chelating agents [85], such as ASB, is crucial for mesopore formation [23,86–88]. An accepted mechanism for ASB-chelate is a condensation reaction. During this reaction, unreacted species (such as OH ligands and other small molecules) can promote the formation of mesopores [86]. An additional contribution to the pore size and pore type is the polymer template of the electrospun fibers [69]. In this case, the template can be removed by applying a heat treatment and form pores and other asperities over the Al<sub>2</sub>O<sub>3</sub>. It should be noted that heat treatment can also alter the physical and chemical properties of Al<sub>2</sub>O<sub>3</sub> nanofibers. This includes the formation of amorphous, semicrystalline, and crystalline Al<sub>2</sub>O<sub>3</sub> [14,15].

In this report, we studied different Al-formulations (e.g., ASBchelate, aluminum nitrate, alumina nanoparticles used as additives, and combinations) as a first step towards the structural design of ANF networks for catalysis. Among the produced ANFs, ASB reveals the highest acidity as determined with NH<sub>3</sub>-TPD. The  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanofibers obtained from ASB are compared with two commercial y-Al<sub>2</sub>O<sub>3</sub> controls, i.e., amorphous and semicrystalline ANFs from ASB.  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanofibers from ASB show similar acidity, if not even better than the commercial counterpart. IR spectroscopy of pyridine is used to identify the type of acid sites present in the ASB ANFs. Density-functional theory (DFT) has been conducted to understand the desorption kinetics of the adsorbed chemical species, such as ammonia (NH<sub>3</sub>) on  $\gamma$ -Al<sub>2</sub>O<sub>3</sub>. Conclusions are drawn regarding NH<sub>3</sub> reaction kinetics and surface desorption mechanisms. We expect the use of these types of AFNs as a dispersing medium for metal or metal oxide nanoparticles, which is very much desired in the field of heterogeneous catalysis.

### 2. Experiments and methods

### 2.1. Electrospinning of Al<sub>2</sub>O<sub>3</sub> nanofibers

ANFs (amorphous, semicrystalline, and crystalline) were prepared using a commercial electrospinning system from IME Technologies (The Netherlands), which was operated utilizing a stainless steel needle of 0.4 mm inner diameter at a separation distance of 12 cm from the aluminum collector plate. Al(NO<sub>3</sub>)<sub>3</sub>·9H<sub>2</sub>O (AN) ACS grade and C<sub>14</sub>H<sub>27</sub>AlO<sub>5</sub> (ASB) technical grade from Alpha Aesar were used to prepare the aluminum stock solutions (Alstock). Nanoparticulated  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> from Sigma-Aldrich (AL) was

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used as an additive. The following compositions were created using the mentioned precursors and additives: ASB, AN, AN-AL, ASB-AL, AN-ASB, and AN-ASB-AL. All these compositions contained polyvinylpyrrolidone (PVP, MW  $\sim$  1,300,000), N, Ndimethylformamide (DMF), and ethanol. The aluminum precursor concentration was 0.14 M. The final concentrations for PVP and DMF were 8.09 mM and 7.2 M for all cases. Samples with more than one aluminum precursor were mixed, maintaining the same Al molar concentration. A summary of prepared precursors and other electrospinning parameters, like voltages and infusion rates, can be found in Table S3. All samples were collected at 298 K and relative humidity of 25%. After fiber deposition, the ANFs were dried in a furnace at 353 K for 12 h to remove the excess solvent. The obtained ANFs (AN, AN-AL, ASB-AL, AN-ASB, AN-ASB-AL) were annealed at 1173 K (1 K/min) for 1 h to obtain  $\gamma$ -Al<sub>2</sub>O<sub>3</sub>. Fibers from ASB were annealed at 873 K (ASB873K) and 1023 K (ASB1023K) at 1 K/min for 1 h to obtain amorphous and semicrystalline ANFs.

### 2.2. Morphological characterization

Scanning electron microscopy (SEM) images of samples AN, ASB, AN-ASB, AN-AL, ASB-AL, and AN-ASB-AL were taken using an FEI Quanta 450 SEM microscope at 10 kV coupled with in-lens detectors. High-resolution (HR)-SEM images of samples AN and ASB1173K were taken using a Zeiss MERLIN SEM microscope operated at 0.65 kV coupled with High-Efficiency Secondary Electron Detector (HE-SE2). SEM-scanning transmission electron microscope (STEM) was recorded at 20 kV. Prior to STEM analysis, samples were sonicated in ethanol. Sample sonication led to the breaking of the ANFs.

### 2.3. Structural characterization

The crystallographic phase of all samples was analyzed by X-ray powder diffraction (D2 PHASER, Bruker) using Cu K $\alpha$  radiation ( $\lambda$  = 1.5418 Å) operated at 30 kV, 10 mA, in the 2 $\theta$  range between 15 and 80°, employing a step size of 0.05° and a scan speed of 0.1°/s. A Si low background sample holder (Bruker) was used for all samples.

#### 2.4. Chemical surface characterization

X-ray photoelectron spectroscopy (XPS) general survey analysis was performed in a Quantera SXM machine from Physical Electronics using monochromated Al K $\alpha$  (1486.6 eV). The ANFs powder samples were fixed on double-sided adhesive carbon tape mounted on a stainless-steel holder. Low energy electron flood gun was used to supply the missing photo- and Auger electrons. The electron binding energies were referenced to aliphatic carbon C 1 s at 284.8 eV. The obtained peaks analysis was made using the PHI Multipak V9.9.0.8 software (Physical Electronics, Inc.).

### 2.5. Pore property and textural characterization

BET surface area, pore-volume, and pore diameter of the ANF samples were determined from the nitrogen adsorption/desorption isotherms at 77 K on a Micrometrics ASAP 2010 instrument. Before the measurement, each sample was evacuated at 473 K for 4 h. The pore size distributions were calculated from the desorption branch of the isotherm using the Barrett-Joyner-Halenda (BJH) method [29]. Commercial AL and  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> PLURALOX SCFa-140 (ALS) from Sasol were used as control during BET measurements.

### 2.6. Mercury intrusion porosimetry

Mesoporous diameter was determined by mercury intrusion porosimetry on a Poremaster PM-33–14 (Quantachrome<sup>®</sup>) equipment. The pore diameter distribution was calculated using Washburn's equation[89,90]:

$$D_{\nu}(r) = \frac{dV_{Hg}}{dP} \left[ \frac{P^2}{2\gamma \text{Cos}\theta} \right]$$

 $V_{Hg}$  stands for the volume of mercury intruded,  $\gamma$  is the fluid surface tension,  $\theta$  is the fluid contact angle, and dP is pressured across the interface.

### 2.7. Acid sites characterization by pyridine adsorption

The nature and strength of LAS and BAS were determined through the adsorption and temperature-programmed desorption of pyridine (called Py hereafter) over the ANFs and commercial AL and ALS. The ANFs were analyzed with IR spectroscopy through in situ transmission on self-supported wafers (4-10 mg, 13 mm of diameter) pressed at 5 t cm<sup>-2</sup> (490 MPa). The wafers were placed into a Pyrex IR cell fitted with water-cooled NaCl windows. More details of the experimental setup can be found elsewere[91]. Before the adsorption experiments, each sample was pretreated in situ at 723 K (10 K/min) for 30 min under He flow (50 sccm), then cooled down to 303 K, and the reference IR spectra of the "clean wafer" was taken. The samples were exposed to a flow of He containing evaporated Py. The physisorbed Py was further removed under flowing He until the spectra of the adsorbed Py remain stable (about 60 min). The thermal programed desorption of Py (TPD) was measured from 303 K to 723 K at 5 K/min in a flow of He (50 ml/min).

The spectra were acquired with a Nicolet Magna 550 FTIR spectrometer with a cryogenic MCT detector (4 cm<sup>-1</sup> resolution, 25 scans). The gas used in this study was high purity grade He (INDURA UHP 99.999%) and was further purified through a molecular sieve (3 Å), and MnO/Al<sub>2</sub>O<sub>3</sub> traps to remove water and oxygen impurities, respectively.

### 2.8. NH3-TPD

NH<sub>3</sub>-TPD experiments were performed using a Micromeritics Autochem II 2910 instrument to measure the sample's total acidity. Prior to NH<sub>3</sub> adsorption, 150 mg of the sample was loaded into a U-shaped quartz reactor and heated from RT to 673 K with 10 K/ min in a flow of He (50 ml/min), held for 30 min at 673 K (to remove any adsorbed species on the surface). After that, the reactor was cooled to 373 K. The sample was saturated with 1% NH<sub>3</sub> in He (50 ml/min) for 120 min at 373 K, followed by helium flushing (50 ml/min) for 60 min at 373 K to remove physisorbed NH<sub>3</sub>. The sample was then heated to 1073 K at a rate of 10 K/min in He flowed (50 ml/min) and held at 1073 K for 30 min for NH<sub>3</sub> desorption. Analysis of the effluent gases was performed with a Quadrupole mass spectrometer (Balzers Omnistar) using m/z = 15. Commercial AL and  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> PLURALOX SCFa-140 (ALS) from Sasol were used as references for comparison.

### 2.9. Computational methods

NH<sub>3</sub> adsorption was studied using periodic DFT-D (Dispersioncorrected Density Functional Theory) calculations with the Vienna Ab Initio Simulation Package (VASP 5.4.4) [92,93]. BEEF-vdW (Bayesian Error Estimation Functional with van der Waals correlation) was employed to also account for van der Waals interactions for all reaction intermediates [94]. The one-electron Kohn-Sham orbitals were expanded on a plane-wave basis with a kinetic energy cut-off of 550 eV for all calculations. Furthermore, the Projector Augmented Wave approximation (PAW) was used [95]. For the Brillouin zone sampling, a 3x3x1 k-point grid was employed and a vacuum of more than 16 Å. Gaussian smearing[92] of 0.1 eV was applied to improve convergence. The geometries were considered converged if the largest force was below 0.03 eV/Å.

Additionally, the convergence criterion for the Self-Consistent electric Field (SCF) problem was set to 10<sup>-6</sup> eV for structural optimizations. Next, for  $\gamma$ -Al<sub>2</sub>O<sub>3</sub>, a periodic (110) surface slab was constructed. The surface is composed of 4 layers of Al<sub>8</sub>O<sub>12</sub> to obtain periodic unit cells terminated with Al-groups with different coordination numbers and surface implantation, shown in Figure S1. Similar model systems were previously employed to study  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> containing model systems [20,96,97,98]. As presented in Figure S1, even chemisorbed water can be removed during a pretreatment at a high temperature above  $\sim$  900 K and relatively low water partial pressures. However, if the pretreatment temperature is lower than  $\sim$  900 K, the  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> surface still contains chemisorbed water. Therefore, we have considered a  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> [110] system with chemisorbed water for NH<sub>3</sub> adsorption. Furthermore, the computational results for NH<sub>3</sub> adsorption on a  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> [110] system without chemisorbed water are presented in the Supporting Information.

For the  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> model systems, Partial Hessian Vibrational Analysis (PHVA) is employed only for the surface species while keeping the rest of the system stationary. The numerical partial Hessian was calculated by displacements in x, y, and z-directions of ± 0.02 Å, and the vibrational modes were extracted using the normal mode analysis as implemented in the post-processing toolkit TAMKIN [99]. The PHVA was used to obtain zero-point corrections and free energy contributions. The Gibbs free energies of adsorption were calculated at various temperatures. In the immobile adsorbate approach applied to chemisorbed NH<sub>3</sub>, a complete loss in translational and rotational entropy of the NH<sub>3</sub> adsorbates upon adsorption or chemisorption on the  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> model is considered. However, at higher temperatures, it is expected that the adsorbed NH<sub>3</sub> can translate more freely over the model surface as barriers for hopping between adsorption sites are hardly activated (10-20 kJ/mol). Therefore, a mobile adsorbate approach has been employed for physisorbed NH<sub>3</sub> molecules, maintaining 2 of their translational degrees of freedom. In other words, whenever one of the NH<sub>3</sub> adsorbate molecules was not fully chemisorbed, the molecule was treated as being physisorbed, maintaining a free-translator in two dimensions. Therefore, the additional translational entropy was then calculated by treating the adsorbed  $NH_3$  species as a two-dimensional gas [100,101,102].

### 3. Results and discussions

### 3.1. $\gamma$ -Al<sub>2</sub>O<sub>3</sub> in the form of nanofibers

The precursor composition of the  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanofibers is varied, intending to achieve the highest acidity and highest surface area. The selected precursors ASB, AN, AL, and their combinations (ASB-AL, AN-ASB, and AN-ASB-AL) are shown in **Table S3**. Among the precursors used to produce ANFs, ASB results in the ideal candidate because it can lead to a sol–gel that can be added directly to the precursor for electrospinning [103]. It is important to note that variations in the precursor composition can alter electrospinning conditions (**Table S3**) [63,83,104–106] in some cases leading to nanofiber instabilities. SEM images of the  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanofibers annealed at 1173 K are presented in Fig. 1. Here, ASB1173K (Fig. 1(**a**)), AN (Fig. 1(**b**)), and their combinations (AN-ASB, Fig. 1 (**c**)), including additives (ASB-AL, AN-AL, AN-ASB-AL) in Fig. 1(**d**-

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Fig. 1. SEM pictures of (a) ASB1173K, (b) AN, (c)AN-ASB, (d) ASB-AL, (e) AN-AL, and (f)AN-ASB-AL ANFs calcined at 1173 K.

f), reveal a non-woven structure alike with some axisymmetric instabilities. The  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanofibers with ASB1173K, AN, and AN-ASB have a fibrous structure with nanofiber diameters of  $83 \pm 11$ , 85 ± 15, and 112 ± 20 nm. Insets in Fig. 1 (a-b) and Figure S2 visualize the nanofiber roughness observed for most of the ANFs in Fig. 1. The roughness can be attributed to the removed organic content after annealing from ASB and AN. The addition of AL to ASB and AN affects the overall ANF morphology. These ANFs are more inhomogeneous than ASB, AN, and AN-ASB. Some agglomerates are found in Fig. 1 (d-f), which are thought to come from the fiber whipping instability during the fly of fibers towards the collector plate. AN-ASB-AL results in nanofibers of 91 ± 29 nm in diameter. Due to their poor fiber characteristics (Fig. 1 (d-e)), ASB-AL and AN-AL have not been further investigated. A STEM image of the commercial AL lacking fibrous morphology[107] is shown in Figure S3 for comparison. Poor fiber characteristics in Fig. 1 (d-e) are attributed to the presence of AL in the electrospinning mixture (Table S3).

We now turn to investigate the structural characteristics of ASB1173K, AN, and AN-ASB calcined at 1173 K with XRD. From the results in Fig. 2(a), it is clear that at 1173 K, the  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> phase is mainly formed. In Fig. 2(b), we also examine the ASB nanofibers over two new temperatures, i.e., 873 and 1023 K, to corroborate the presence of the  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> found at 1173 K in Fig. 2(a). ASB thermally treated at 873 K and 1023 K do not completely transform into the  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> crystallographic phase. The formation of an amorphous Al<sub>2</sub>O<sub>3</sub> is encountered at 873 K, whereas peak-broadening in XRD has been found more pronounced at 1023 K, indicating a semicrystalline phase [15,108–110]. With this structural analysis, we can identify the temperature range for either amorphous and semicrystalline ASB ANFs, and crystalline  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanofibers for the ASB precursor. In Fig. 2(a) and Fig. 2(b), AL is used as a reference and matched with the ICDD 29-1486 card showing peaks located at  $2\Theta = 22^\circ$ ,  $35^\circ$ ,  $39^\circ$ ,  $42^\circ$ ,  $48^\circ$ ,  $63.3^\circ$ ,  $69^\circ$ , which corresponds to (111), (220), (311), (222), (400), (511), and (440) crystal planes from  $\gamma$ -Al<sub>2</sub>O<sub>3</sub>. From the XRD results, it is fair to say



Fig. 2. XRD diffraction patterns of (a) ANFs obtained at 1173 K with various precursors (AN, AN-ASB) and (b) ASB ANFs annealed at 1173, 1023, and 873 K. AL is used for comparison.

that the ANFs in Fig. 2(a) is composed of  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> phase. It should be noted that for AL reference, another peak appears at 36.8° label with (104) crystal plane, which matches the ICDD 42–1468 card data and therefore corresponds to  $\alpha$ -Al<sub>2</sub>O<sub>3</sub>.

To estimate the acid site distribution per unit volume, we introduce first the results from the textural analysis performed with BET for samples ASB1173K, AN, AN-ASB, and thermally treated ASB at 873 K (ASB873K), and 1023 K (ASB1023K) in Tables 1 and 2. The highest surface area is obtained for ASB873K and ASB1023K with 234 and 200 m<sup>2</sup>/g, respectively, followed by ASB1173K with 180 m<sup>2</sup>/g. Other formulations like AN and AN-ASB remain below the 77 m<sup>2</sup>/g. Compared to commercial  $\gamma$ -Al<sub>2</sub>O<sub>3</sub>, ASB1173K has a higher surface area than AL but not ALS. The effect can be attributed to sintering or phase transformation for AL,[31] making ASB of value for chemical reactions where  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> is required [42]. These findings are significant because it shows that the electrospun ASB precursor can considerably increase the surface area, even higher than commercial  $\gamma$ -Al<sub>2</sub>O<sub>3</sub>, like AL (114.5 m<sup>2</sup>/g) and other ANFs reported in the literature (Table S1). Additional evidence showing that the ASB precursor increases the surface area is presented in Table 2. In this case, the ASB1173K nanofibers are compared with

Table 1 Fiber diameter, surface area, and total acidity of  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> fibers obtained at 1173 K using different precursors.

Samples annealed	Surface area	Total acidity	Total acidity
at 1173 K	(m²/g)	(μmol/g)	(µmol/m²)
ASB1173K	180.8	134.3	0.7
AN	63.7	29.7	0.5
AN-ASB	53.3	24.2	0.45
AL	114.5	105.0	0.9
ALS	217.6	212.2	1.0

drop-casted ASB annealed at 1173 K (hereafter ASB1173K-DC). ASB1173K-DC results in  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> but lacks a nanofiber-like structure (Figure S3). Surface area measures evidence that the ASB1173K nanofibers retain a higher surface area than ASB1173K-DC in Table 2. The BET results are also in agreement with the total surface area found for ASB1173K (158  $m^2/g$ ) and AL (115 m<sup>2</sup>/g) measured with mercury (Hg) intrusion. Interestingly, the mean pore diameter for Hg intrusion has been found higher for ASB1173K (ca. 4  $\mu$ m) than AL (ca. 150 nm). Therefore, it is fair to say that macropores are formed thanks to the nonwoven fiber structure of ASB1173K (Fig. 1(a)). AL does not count with such structural characteristics, as displayed in Figure S3. To this end, the textural properties of the intertwined fibrous network for sample ASB1073K after pressing (3 t/cm<sup>2</sup>) (named ASB1023K\*) is also assessed in Table 2 to corroborate if changes in the ANFs structure might change the surface area as measured with BET. From the results, it is observed that pressing does not change the textural properties of ASB1073K. Similarities characteristics are expected for the other ANFs in Tables 1 and 2.

Among the ANFs from Tables 1 and 2, it is clear that ASB873K, ASB1023K, and ASB1173K ANFs have the highest specific surface area, even one of the highest reported for nanofibers (Table S1). An in-depth analysis using the BET isotherms from Fig. 3 is assessed to generate insights into the pore type and pore size distribution in ASB ANFs. For this study, ASB is contrasted with  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanofibers types (AN and AN-ASB), ASB873K, ASB1023K, and commercial  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> (AL and ALS). Fig. 3 shows two different sets of adsorption–desorption isotherms. First, pretreated ANFs at 1173 K, i.e., ASB1173K, AN, and AN-ASB in Fig. 3(a). Second, ASB ANFs, i.e., ASB873K, ASB1023K, and ASB1173K in Fig. 3(c), which figure aim to generate insights on the effect of temperature in ASB. Fig. 3(a,c) showed hysteresis loops in the multilayer step associated with capillary condensation. Fig. 3(a) shows that the isotherm of sample ASB1173 K and ALS are of type IV for meso-

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#### Table 2

Fiber diameter, surface area, total acidity, and pore size of Al<sub>2</sub>O<sub>3</sub> fibers obtained at 873, 1023, and 1173 K using ASB as the precursor. \*ASB1023K pressed using 3 t/cm<sup>2</sup>.

Sample	Surface area (m <sup>2</sup> /g)	Pore size (nm)	Total acidity (µmol/g)	Total acidity ( $\mu mol/m^2$ )
ASB873K	234.5	6.7	141.3	0.6
ASB1023K	200.5	6.4	139.6	0.7
ASB1023K*	198.2	6.7	-	-
ASB1173K	180.8	7.4	134.3	0.7
ASB1173K-DC	100.3	7.5	-	-



Fig. 3. Adsorption-desorption isotherms and pore size distribution for (a, b) ASB1173K, AN, AN-ASB, AN-ASB-AL ANFs obtained at 1173 K. (c, d) ASB873K, ASB1023K, and ASB1173K. AL and ALS are included for comparison.

pores with H2 hysteresis[111]. In the same figure, the samples AN and AN-ASB and AL showed type II isotherms with H3 hysteresis shape, suggesting slit-shaped pores of non-rigid aggregates of plate-like particles [112,113]. The pore size distribution curves in Fig. **3(b)** corroborate wider pore bodies for most of the  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanofibers, excepting ASB that shows a narrow distribution between 7 and 8 nm very much comparable to ALS with 8 nm. It is clear that ASB ANFs have lower incremental pore volume than ALS Fig. **3(b)** but with the advantage of macropores formation (Fig. 1(**a**)). With such characteristics on hand, the ASB ANFs can be cataloged as a material that combines mesoporosity [10,28,114–117] and microporosity in one.

Results for ASB873K and ASB1023K in Fig. **3(c)** show great similitude to ASB1173K, where the adsorption-desorption isotherms reveal the type IV with H2 behavior. Differences in the hysteresis loop between ASB873K, ASB1023K, ASB1173K could be attributed to the pore broader bottleneck present at lower temperatures in Fig. **3(d)**. Similar porosity is maintained for ASB1023K\* in Table 2 after compression without compromising the surface area. As temperature increases to 1173 K, narrow pores are observed.

From the ANFs, ASB has a narrower pore size distribution with the highest amount of mesopores.

We investigated the porosity formed throughout the ASB ANFs with STEM to support our different temperature experiments from Fig. 3(c). The results are presented in Fig. 4. STEM images in Fig. 4(a-c) for ASB873K, ASB1023K, and ASB1173K are recorded in dark field mode. Samples in the row below (Fig. 4(d-f)) follow the same order as in Fig. 4(a-c). The bright-field image in Fig. 4(d) corresponds to sample ASB873K and reveals a pronounced contrast, where pores throughout the ANFs are seen (yellow arrows). These results confirm that the annealing temperature decreases porosity, particularly when comparing STEM images Fig. 4(a, d) with Fig. 4 (**b**, **c**). The reduction in porosity in Fig. 4(**c**) can be attributed to sintering effects [28]. Furthermore, SEM images for ASB1023K in Fig. 4(e-f) help to corroborate surface roughness (dashed ellipses), which is seen in the form of wrinkles found in Fig. 1. It should be noted that all ANFs in Fig. 4 have been subjected to sonication before analysis, and thus, it is expected to observe broken ANFs. To this end, the purity of ASB ANFs is determined by analyzing the chemical surface composition of ASB873K and ASB1173K with

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Fig. 4. STEM images for ASB873K, ASB1023K, and ASB1173K ANFs.

XPS. XPS ensures that the produced ASB aluminas between 873 K and 1173 K do not contain residues that might affect the alumina nature (e.g., acid nature). In this case, a possible contaminant is nitrogen species due to PVP. The general survey of the samples revealed only the presence of aluminum and oxygen (Figure S4).

### 3.2. The nature of acidity sites in $\gamma$ -Al<sub>2</sub>O<sub>3</sub> and Al<sub>2</sub>O<sub>3</sub> nanofibers

Py is an appropriate probe molecule to study the nature of BAS (protonic acidity) and LAS surface acid sites (aprotic acidity) [42,118]. ASB ANFs have been analyzed with Py adsorption since ASB ANFs showed desirable textural properties in Tables 1 and 2. Commercial AL and ALS are also used for comparison during Py-FTIR experiments. Fig. 5(a) shows the FTIR spectra of Py adsorbed on ASB873K, ASB1023K, ASB1173K, AL, and ALS at 303 K. All the samples show bands at 1446, 1577, and 1614 cm<sup>-1</sup> attributed to Py adsorbed on LAS. The LAS of alumina are produced partly by uncoordinated Al<sup>3+</sup> and by cation vacancies exposed on the surface [119]. The band around 1594 cm<sup>-1</sup> is assigned to hydrogen-bonded pyridine [120]. As other authors report, [121] this band completely disappears after heating at 373 K (Figure S5). The signal at

1491 cm<sup>-1</sup> is attributed to Py adsorbed on both Lewis and BAS. However, in our alumina, the contribution to the BAS band is only given by LAS. The absence of the signal at 1540 cm<sup>-1</sup> of the protonated Py (PyH<sup>+</sup>) suggests that BAS are not present in the  $\gamma$ -Al<sub>2</sub>O<sub>3</sub>[20] nor amorphous and semicrystalline nanofibers. In other words, the OH is not strong enough to protonate the Py[122]. The effect of Py adsorption on the OH group bands is used to characterize further and identify the acid groups. In this case, the OH can be perturbed by the direct hydrogen-bonded pyridine (1594 cm<sup>-1</sup>) and via hydrogen bonding of the Py ring (adsorbed on LAS) next to an OH adjacent group [120]. Fig. 5(b) shows the difference spectra in the high-frequency region recorded at 303 K after Py adsorption. The variation in the OH bands is clear by the negative bands at around 3850 and 3670 cm<sup>-1</sup>. The hydrogen bonding is evidenced by the positive broad bands around 3500-3400 cm<sup>-1</sup>. These results further indicate that the Py is adsorbed on LAS and hydrogen-bonded to the surface. For comparison, the IR spectra in the high-frequency region in the absence of Py adsorption at 723 K are presented in Figure S6. The results reveal the presence of chemisorbed water in  $\gamma$ -Al<sub>2</sub>O<sub>3</sub>.



Fig. 5. (a) FTIR spectra after Py adsorption and (b) FTIR high-frequency region spectra after Py adsorption on ASB873K, ASB1023K, ASB1173K, AL, and ALS at 303 K.

To this end, it is important to summarize previous results from Fig. 3, Fig. 4, and Fig. 5. The results reveal two main effects dominating in ASB873K, ASB1023K, ASB1173K. First, the mesoporous character of the ASB nanofibers (Fig. 3), which formation can be correlated to a condensation reaction [86]. PVP (main nanofiber component) used as a template might also introduce mesopore formation in the nanofibers after removal. Small pores can be also be found in Fig. 4 for ASB873K, ASB1023K, ASB1173K. As the temperature increases for ASB873K, ASB1023K, ASB1173K. As the temperature increases for ASB873K, ASB1023K, ASB1173K, more dense ANFs are found. AFNs in Fig. 4 suggests a reduction in surface area, as shown in Table 2. Regardless of the ASB ANF type, the nature of the acid sites prevails to be prominently LAS, as shown in Fig. 5. Similar acid sites have been found for AL and ALS in Fig. 5.

### 3.3. TPD-NH<sub>3</sub> of $\gamma$ -Al<sub>2</sub>O<sub>3</sub> and Al<sub>2</sub>O<sub>3</sub> nanofibers

TPD is used to determine the total acidic sites using NH<sub>3</sub> as a probe molecule. In Fig. 6, the NH<sub>3</sub>-TPD profiles are presented for ASB1173K, ASB1023K, ASB873K ANFs, and AL. The number of acid sites for ASB ANFs and commercial  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> is presented in Table 1 and Table 2. In these tables, the highest content of acid sites has been estimated for ALS, followed by ASB873K, ASB1023K, ASB1173K, AL, AN, and AN-ASB. For the  $\gamma$ -Al<sub>2</sub>O<sub>3</sub>, the acidity decreases as follows ALS(212.2 µmol/g) > ASB1173K(134 µmol/g) > AL(105 µmol/g) > AN(29.7 µmol/g) >AN-ASB(24.2 µmol/g). Most



Fig. 6.  $\rm NH_3\text{-}TPD$  profiles of ASB ANFs obtained at 873, 1023, and 1173 K. AL is used as a control.

of the ANFs show a relatively low amount of acidic sites, except ASB. From these results, the acidity found for the thermally treated ASB ANFs can be directly dependent on the temperature and crystallinity of the formed  $Al_2O_3$  and not on other impurities (**Figure S4**). It has been shown that acidity decreases by increasing the crystallinity of  $Al_2O_3$  [98]. Following the same analogy, the decreased acidity of ASB ANFs can be generated by the loss of defects present in the structure due to crystallinity change from amorphous to  $\gamma$  phase. Therefore, it is reasonable to find a higher content of acid sites for amorphous, semicrystalline  $Al_2O_3$  nanofibers than  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanofibers.

From the NH<sub>3</sub>-TPD results, it is clear that ASB has the highest acid site content among the ANFs. The nature of the acid sites can be attributed to LAS by Pyridine analysis.(Fig. 5(a)). With NH<sub>3</sub>-TPD information, we can estimate the acid site distribution per unit volume of the ANFs (Table 2). The ASB ANFs remain the highest reported in the literature (**Table S1**), with a total acidity of 0.7  $\mu$ mol/m<sup>2</sup>. The other ANFs fall below 0.7  $\mu$ mol/m<sup>2</sup>. Compared to commercial catalysts, the total acidity for ASB1173K seems to be close to AL (0.9  $\mu$ mol/m<sup>2</sup>) and ALS (1  $\mu$ mol/m<sup>2</sup>). The results are quite interesting because ASB ANFs combine most of the desired characteristics of an acid catalyst but have additional structural dimensions in the form of non-woven nanofibers, a feature that is very much appreciated in catalysis [123].

### 3.3.1. Acid site strength in $\gamma$ -Al<sub>2</sub>O<sub>3</sub> and Al<sub>2</sub>O<sub>3</sub> nanofibers

We then proceed to understand the acid strength distribution with NH<sub>3</sub>-TPD. The NH<sub>3</sub>-TPD results have been analyzed using a Gaussian distribution function. The reason for selecting a Gaussian function is because it is well accepted to provide more reliable and consistent desorption energy data for alumina [124]. In particular, NH<sub>3</sub>-TPD for  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> can be described as a linear combination of three Gaussian curves [125]. Therefore, we proceed to deconvolute all measured NH<sub>3</sub>-TPD profiles in three Gaussian peaks. Each of these peaks were assigned over three regions corresponding to weak (373-433 K), medium (433-533 K), and strong acid sites (533–773 K). Weak (I), medium (II), and strong (III) acid sites are colored in brown, light blue, and green in Fig. 6. The Py-FTIR and NH<sub>3</sub>-TPD results suggest that weak LAS contributes to the TPD peak[126] located between 373 and 433 K since hydrogen bonded desorb at temperatures below 373 K [127,128,129]. On the other hand, medium and strong LAS might be expected for an NH<sub>3</sub>-TPD temperature range between 433 and 773 K (Fig. 6(a) and Figure S5) [127–130]. It should be mentioned that acidity has tremendous repercussions during chemical transformation. Some examples in the field of heterogeneous catalysis are listed in Table S2. Understanding how molecular adsorbates, such as NH<sub>3</sub>, interact with  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> can help generate insights into acid sites mediated reaction mechanisms in  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> [20].

#### 3.3.2. NH<sub>3</sub> desorption kinetics

We can further generate valuable insights into the overall desorption kinetics with DFT on a  $\gamma$ -Al<sub>2</sub>O<sub>3</sub>(110) model system with one chemisorbed H<sub>2</sub>O molecule [96,97,98]. On this model system, the presence of chemisorbed and adsorbed H<sub>2</sub>O is studied first (**Figure S1**) to verify if H<sub>2</sub>O is eliminated during the temperature pretreatment at 673 K or higher temperatures. After such treatment, we can still expect some chemisorbed water on nanofibers and commercial  $\gamma$ -Al<sub>2</sub>O<sub>3</sub>, also confirmed with FTIR in **Figure S6**. Therefore, we consider the bare  $\gamma$ -Al<sub>2</sub>O<sub>3</sub>(110)-model system with one chemisorbed water as representative of the state of  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> before NH<sub>3</sub> adsorption. Moreover, 4 different exposed Al-sites are on the surface (Fig. 7), labeled as empty sites \*1, \*2, \*3, and \*4. This model system thus contains various relevant adsorption sites that can be representative for the  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> ANFs. The Al-site \*1 is coordinated to 3 oxygen atoms, and \*2, is coordinated to 4 oxygen



**Fig. 7.** Schematic reaction pathway of plausible desorption pathways starting from a  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> [110] model system with chemisorbed water. The different NH<sub>3</sub> adsorption sites with their respective desorption temperature T<sub>des</sub>, (K, red) and  $\Delta$ H<sub>des</sub> (kJ/mol, black). Atomic color codes: Al (gray), O (red), N (blue), H (white), the periodic repeating unit (black rectangle). (For interpretation of the references to color in this figure legend, the reader is referred to the web version of this article.)

atoms, while \*3 and \*4 are coordinated to 5 oxygen atoms. In fact, \*3 and \*4 could be considered active sites of great similitude. It should be noted that the Al-site coordination to oxygen atoms might vary for the ASB-derived  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanofibers or commercial catalysts. In other words, each  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> will have a different population and distribution of adsorption sites. Therefore, the current computational study can provide understandings into the NH<sub>3</sub> adsorption and desorption on different Al-sites.

The expected adsorption configuration for NH<sub>3</sub> is given in Fig. 7. The configuration with adsorbed NH<sub>3</sub> group is labeled according to the sites NH<sub>3</sub> occupies. In the following, we refer to the possible adsorption configurations with a number code (left upper side of each panel, e.g., 124). In 124, the adsorption configuration is with 3 NH<sub>3</sub> molecules. Most of the contributions during NH<sub>3</sub> desorption might be expected for LAS and BAS. However, when studying various BAS at high NH<sub>3</sub> coverage (Fig. 7), the typical adsorption enthalpies observed were between -10 and -15 kJ/mol, which would correspond with desorption temperatures below 200 K at an NH<sub>3</sub> partial pressure of 100 Pa. Experimentally, only LAS and hydrogenbond Py have been observed on  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> as identified with Py-FTIR and in agreement with our model, NH<sub>3</sub> adsorbed by hydrogenbond is expected to desorb below the 373 K, if any. For the analysis, the NH<sub>3</sub> partial pressure during TPD is estimated at 100 Pa for the chemisorbed water model system in Fig. 7. However, it should be noted that a lower NH<sub>3</sub> partial pressure results in lower desorption temperatures, which you can expect for nonchemisorbed water. In supporting information, computational results are also presented for a  $\gamma$ -Al<sub>2</sub>O<sub>3</sub>(1 1 0)-model system without chemisorbed water (Figs S7, S8, and S9, Table S4).

The stepwise desorption of NH<sub>3</sub> can be determined, as shown in Fig. 7. However, if we consider the different sites at low loading, the most strongly adsorbing Al-site is \*1, which has an adsorption enthalpy ( $\Delta H_{ads}$ ) of ca. -185.6 kJ/mol and thus a desorption enthalpy ( $\Delta H_{des}$ ) of 185.6 kJ/mol (i.e.,  $-\Delta H_{ads} = \Delta H_{des}$ ). This high NH<sub>3</sub> adsorption energy can be understood since \*1 is the Al-site with the lowest oxygen coordination number (CN<sub>Al-\*1</sub> = 3). The

other considered Al-sites in the  $\gamma$ -Al<sub>2</sub>O<sub>3</sub>(110)-model system (\*2, \*3, and \*4) have a higher oxygen coordination number (CN = 4 or 5), which results in less strongly adsorbed NH<sub>3</sub> molecules with  $\Delta$ H<sub>des</sub> below 145 kJ/mol. Adsorption of an NH<sub>3</sub> molecule over \*4 results in an  $\Delta$ H<sub>des</sub> = 122.7 kJ/mol, and for \*2, we find  $\Delta$ H<sub>des</sub> = 14 5.1 kJ/mol. The  $\Delta$ H<sub>des</sub> is estimated using the mobile adsorbate approach for physisorbed NH<sub>3</sub>, while the immobile adsorbate approach is taken for chemisorbed NH<sub>3</sub> (only for \*1).

To gain insight into the overall desorption kinetics process of TPD on  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> (110), we require an understanding of the subsequent NH<sub>3</sub> desorption. This implies that after desorption in Fig. 7, there is an additional relocation of NH3 until exhaustion from the  $\gamma\text{-}Al_2O_3\ (1\,1\,0)$  surface. Therefore, the thermodynamic stability of NH<sub>3</sub> over  $\gamma$ -Al<sub>2</sub>O<sub>3</sub>(110) at different ammonia partial pressures  $(p_{NH_2})$  and temperature is presented in **Figure S8**. In this figure, it is possible to optimize the  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> (110) surface with two additional NH<sub>3</sub> adsorbates. However, desorption of the first two NH<sub>3</sub> molecules happens easily, with average  $\Delta H_{des}$  near 0 kJ/mol [129]. Hence, model systems with fewer NH<sub>3</sub> molecules are considered to be more suitable to study subsequent NH<sub>3</sub> desorption. In this approach, NH<sub>3</sub> is loaded over Al-sites, as shown in Fig. 7. From the analysis, we derive the free energy difference for various temperatures and an NH<sub>3</sub> partial pressure of 1 mbar in Table 3. The most likely desorption pathway takes place by initial removal of hydrogen-bonded NH<sub>3</sub>, i.e. **124**  $\leftrightarrow$  **124** + NH<sub>3</sub>, followed by NH<sub>3</sub> on LAS; 124  $\leftrightarrow$  12 + NH<sub>3</sub>  $\leftrightarrow$  1 + 2NH<sub>3</sub>  $\leftrightarrow$  empty + 3NH<sub>3</sub> and **124**  $\leftrightarrow$  **24** + NH<sub>3</sub>  $\leftrightarrow$  **2** + 2NH<sub>3</sub>  $\leftrightarrow$  **empty** + 3NH<sub>3</sub>. If for the last desorption step from the most stable physisorbed NH<sub>3</sub>, i.e.  $1 \leftrightarrow empty + NH_3$ , a lower NH<sub>3</sub> pressure of 0.25 mbar is assumed, the desorption temperature lowers from 739 K (1 mbar) to 703 K (0.25 mbar) irrespective of the presence of chemisorbed water. However, there is another desorption pathway very likely, suppose that the chemisorbed NH<sub>3</sub> at \*1 is desorbed first, requiring only a desorption enthalpy of 105.7 kJ/mol and this step becomes already exergonic at 479 K. Therefore, it is clear that at high NH<sub>3</sub> coverage of our model system, even chemisorbed NH<sub>3</sub> can desorb first. This

### Table 3

Most likely, desorption pathways of NH<sub>3</sub> starting from 124 in Fig. 7 for mobile adsorbates at  $p_{NH_3}$  = 100 Pa.

Reaction	T <sub>des</sub> (K)	$\Delta H_{des}$ (kJ/mol)	$\Delta G_{des}$ (kJ/mol)					
			300 K	400 K	500 K	600 K	700 K	800 K
$124 \leftrightarrow 12 + \text{NH}_3$	441	97.8	31.0	8.9	-13.1	-34.9	-56.5	-80.0
$124 \leftrightarrow 24 + \text{NH}_3$	479	105.7	39.0	17.1	-4.7	-26.2	-47.5	-68.5
$124 \leftrightarrow 14 + \text{NH}_3$	515	111.2	46.2	24.6	3.1	-18.1	-39.2	-60.1
$12 \leftrightarrow 1 + \text{NH}_3$	354	77.5	11.7	-10.1	-31.7	-53.1	-74.2	-95.1
$12 \leftrightarrow 2 + NH_3$	550	118.0	53.2	31.7	10.4	-10.6	-31.3	-51.9
$14 \leftrightarrow 1 + \text{NH}_3$	300	64.1	-3.4	-25.8	-48.0	-69.9	-91.5	-112.9
$14 \leftrightarrow 4 + \text{NH}_3$	563	127.0	59.0	36.4	13.9	-8.3	-30.2	-52.0
$24 \leftrightarrow 2 + NH_3$	510	110.1	45.0	23.4	2.0	-19.3	-40.4	-61.3
$24 \leftrightarrow 4 + NH_3$	600	132.5	66.0	43.8	21.7	-0.2	-22.0	-43.6
$1 \leftrightarrow \text{empty} + \text{NH}_3$	739	173.6	101.5	77.7	54.3	31.3	8.6	-13.8
$2 \leftrightarrow \text{empty} + \text{NH}_3$	565	145.1	67.3	41.5	16.1	-8.9	-33.7	-58.1
$4 \leftrightarrow \text{empty} + \text{NH}_3$	486	122.7	46.4	21.2	-3.6	-28.0	-52.1	-75.8

would then yield structure 24, from which the NH<sub>3</sub> group at position \*4 desorbs at 510 K ( $p_{NH_3}$  = 100 Pa), which can be followed by NH<sub>3</sub> desorption from \*2 at 565 K. While the desorption temperature for the reaction sequence  $124 \leftrightarrow 24 + \text{NH}_3 \leftrightarrow 2 + 2\text{NH}_3$ - $\leftrightarrow$  empty + 3NH<sub>3</sub>, are thus respectively 479, 510 and 565 K at an NH<sub>3</sub> partial pressure of 100 Pa. Lowering the NH<sub>3</sub> partial pressure to 10 Pa, results in lowered desorption temperatures by about 40 K, i.e. 440, 468, and 525 K. The latter 3 temperatures agree well with the temperature ranges that were used to fit Gaussians to the experimental TPD data, i.e., 373-433 K, 433-533 K, and 533-773 K (Fig. 6). However, it should be noted that compared with the experiment data, we would need to know the distribution of adsorption sites, especially the % of \*1 sites. These threefold coordinated Al-sites can have the highest desorption at low NH<sub>3</sub> coverage enthalpies, which ultimately result in the highest desorption temperatures.

In general, the extracted experimental desorption kinetics typically varies between  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> and might contain another site distribution present in our atomistic model. Nevertheless, the model may be compared with the experimental conditions of the NH<sub>3</sub>-TPD, by assuming that at the begging of the TPD analysis, all the different acid sites of the alumina are fully covered (coverage ( $\theta$ ) of NH<sub>3</sub> on alumina is  $\theta$  = 1), which is in agreement with the protocol followed by the theoretical calculations by determining one NH<sub>3</sub> molecule per active site.

Once the desorption temperature range for the acid site range is defined, a kinetic order analysis of multisite NH<sub>3</sub>-TPD[131] is employed. This model is based on the linearization of the integral function of the Polanyi-Wigner equation. It is worth mentioning that, in our case, the empirical desorption energy  $(E_d)$  values correspond to the apparent desorption energy due to the exclusion of the readsorption processes in the mathematical model, which is highly possible at low heating rates. Moreover, a pre-exponential factor of  $10^{11} \text{ s}^{-1}$  is assumed (value reported for  $\gamma$ - Al<sub>2</sub>O<sub>3</sub>) [132]. By following the regression procedure outlined for different desorption reaction orders in **Table S5** at a coverage  $(\theta) = 1$  (explained above in the text), we found that the NH<sub>3</sub>-TPD of ASB1173K, AL, and ALS follow zeroand first-order desorption kinetics [131]. The approach uses the experimentally recorded NH<sub>3</sub>-TPD from Fig. 6 for  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> only. The desorption energy for each of the acid types assigned can be estimated using the proposed empirical approach [131]. For the approach, the apparent desorption energy (E<sub>d</sub>) for ASB1173K, AL and ALS can be correlated to  $\Delta H_{ads}$  by the equation  $[q_{ad} = \Delta H_{ads}^0 = E_d + 1/2 \text{ RT}$ , [133] leading to an estimation of the desorption enthalpy, i.e.  $\Delta H_{ads} = -\Delta H_{des}$ . The averaged  $E_d$  results from the temperature range for weak, medium, and strong acid sites.

As it is seen from **Table S5**, different desorption orders are observed for the different acid types. The difference may be attributed to different desorption kinetics due to the different distribution of acid type in  $\gamma$ -Al<sub>2</sub>O<sub>3</sub>. A first-order desorption kinetic model is most appropriate for weak and medium sites based on the highest R<sup>2</sup> value (Table S5) and literature [132–136]. To illustrate our kinetic order calculation, the linear regression of the function  $\ln(\theta_i, \theta_i - \Delta \theta)$  vs. inverse temperature (1/K) is plotted in **Figure S10** [133]. With such an approach, the calculated E<sub>d</sub> interval for the weak (374–433 K) and medium (433–532 K) acid site is  $\sim$ [-96, -106] kJ/mol and [-106, -132] kJ/mol, respectively. Even with the variation in acid site distribution, these E<sub>d</sub> results are comparable to Table S4 and show increased desorption energies at higher temperatures. Then the, zero-order desorption kinetic model resulted in a better fit for the mathematical modeling of strong acid sites (533–773 K) with the highest desorption energies and temperatures (Table S5 and Figure S10). The zero-order desorption kinetic can be attributed to NH<sub>3</sub> readsorption, which significantly lowers the kinetic order close to zero [129]. The derived apparent desorption energy interval for strong acid sites is [-115, -171] kJ/mol (Table S5). For comparison, the estimated values for the apparent desorption energy interval for n = 0 and n = 1are presented in Table S6.

Finally, from the desorption kinetic study, we can derive the following conclusions: (i) the R<sup>2</sup> results in the supporting information support the kinetic desorption order (n) = 0 or 1. (ii) The simulated desorption kinetics process of TPD is derived from 4 different desorption steps. We can compare the final desorption energy for an empty surface with these desorption steps, assuming a surface coverage close to zero. For low coverage, the most stable adsorbed/physisorbed NH<sub>3</sub> is \*1 with an estimated  $\Delta H_{des}$  of 173.6 kJ/mol for physisorbed NH<sub>3</sub> at 739 K for the mobile adsorbate approach, while for the standard immobile adsorbate approach, this would be a  $\Delta H_{des}$  of 176.1 kJ/mol at 862 K. Assuming in the mathematical model for desorption a reaction order n = 0, a calculated  $\Delta H_{des}$  of around 176 kJ/mol is obtained at around 800 K; which lies actually in between the mobile and immobile adsorbate approach [90]. There is thus a close similarity between our mathematical model and the ab initio calculations.

The results for ASB-derived  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanofibers have comparable kinetic desorption properties to AL and ALS. The advantages of nanofibers are foreseen microporosity, acidity, and relatively high surface area among fibrous materials (Table 1). ASB nanofiber properties can be of great interest in catalysis. Several methods have been used to synthesize ANFs, including sol–gel and solvothermal, amongst others (Table 1). We aim to position electrospinning as a synthesis method of catalytic supports, where the fiber's macroporosity can facilitate reactants and product diffusion during a catalytic reaction. Additionally, the small diameter of the nanofibers makes short diffusion pores, ensuring the absence of

diffusional limitations. Electrospinning and any other of their configurations can provide the tools for developing a structured catalyst where acidity and porosity can be controlled. The ultimate alumina material will be useful for specific chemical reactions (**Table S3**).

### 4. Conclusions

 $\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanofibers with high acidity and surface area have been prepared using electrospinning from different Al<sub>2</sub>O<sub>3</sub> precursors. The surface area for these non-woven nanofiber specimens, measured with BET, indicates the presence of pores in the range of 4.5–10 nm. The synthesized  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanofibers have a tunable surface area in the range of 180–235 m<sup>2</sup>/g and acidity of 0.6–0.7  $\mu$ mol/  $m^2$  with ASB Al<sub>2</sub>O<sub>3</sub>/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> the best among the other ANFs. For ASB  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanofibers, macroporosity is evidenced (ca. 4  $\mu$ m). Furthermore, ASB γ-Al<sub>2</sub>O<sub>3</sub> nanofibers reveal LAS prominently. DFT calculations provided fundamental insight into the adsorption/ desorption thermodynamics during NH<sub>3</sub> adsorption/desorption and clearly showed increasing desorption energies with increasing temperature. Furthermore, comparing empirical mathematical modeling and experiments helps create a desorption map for weak, medium, and strong acid sites. This work forms a basis for further utilization of electrospun alumina nanofibers in the field of heterogeneous catalysis.

### **Declaration of Competing Interest**

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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### Appendix A. Supplementary material

Supplementary data to this article can be found online at https://doi.org/10.1016/j.jcat.2021.11.019.

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