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## Performance of a Series of Polishing Ponds in the Treatment of Sanitary Sewage<sup>\*</sup>

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Abstract: the main objective of this research was to evaluate the functioning of a system of polishing ponds on a pilot scale in the post-treatment of urban sewage discharged from an up-flow anaerobic sludge blanket reactor and followed by a submerged aerated filter. The following variables were analyzed: transparency, temperature, dissolved oxygen (DO), pH, alkalinity, biochemical oxygen demand (BOD), chemical oxygen demand (COD), total Kjeldahl nitrogen (TKN), ammonia (NH<sub>3</sub>), organic nitrogen, nitrate (N-NO<sub>3</sub>), total phosphorus (TP), orthophosphate ( $PO_4^{3}$ ), total suspended solids (TSS) and chlorophyll-a. In addition, the planktonic communities were also identified and quantified. During the study period, the pond system registered the following mean and standard deviation of the removal efficiencies: 32.9±31.7% of BOD, 26.5±33.9% of COD, and 29.0±49.6% of TSS; good performance was observed in the removal of nitrogen compounds, and the following results were obtained: 58.4±28.1%, 87.5±15.4%, 24.4±42.6%, and 9.4±51.8%, respectively for TKN, NH<sub>3</sub>, organic nitrogen, and N-NO<sub>3</sub>; and 26.9±25.8 of TP and 34.3 $\pm$ 32.7% of PO<sub>4</sub><sup>3</sup>. During the research period, the planktonic community was represented by the following classes: Chlorophyceae, Euglenophyceae, Cyanobacteria, Cryptophyceae, Zygnemaphyceae, Chrysophyceae, and Dinophyceae; concurrently, the zooplankton registered low densities and was represented by the Rotiferous, Copepod, and Cladocera groups. The results help us understand the performance of polishing ponds in treating sanitary effluents.

Key words: water quality; pollutant removal; stabilization ponds; sanitary effluent treatment

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## *Rendimiento de una serie de estanques de pulido en el tratamiento de aguas residuales sanitarias*

Resumen: el objetivo principal de esta investigación fue evaluar el funcionamiento de un sistema de lagunas de pulimento a escala piloto en el postratamiento de aguas residuales urbanas, descargadas de un reactor anaerobio de flujo ascendente con manto de lodos y seguido de un filtro aireado sumergido. Se analizaron las siguientes variables: transparencia, temperatura, oxígeno disuelto (OD), pH, alcalinidad, demanda bioquímica de oxígeno (DBO), demanda química de oxígeno (DQO), nitrógeno total Kjeldahl (NKT), amonio (NH3), nitrógeno orgánico, nitrato (N-NO3), fósforo total (PT), ortofosfato (PO43-), sólidos totales en suspensión (SST) y clorofila-a. Además, se identificaron y cuantificaron las comunidades planctónicas. Durante el periodo de estudio, el sistema de estanques registró las siguientes medias y desviaciones estándar de las eficiencias de eliminación 32,9±31,7% de DBO, 26,5±33,9% de DQO y 29,0±49,6% de SST. Se observó un buen rendimiento en la eliminación de compuestos nitrogenados, obteniéndose los siguientes resultados 58,4±28,1%, 87,5±15,4%, 24,4±42,6%, y 9,4±51,8%, respectivamente para TKN, NH3, nitrógeno orgánico, y N-NO3; y 26,9±25,8 de TP y 34,3±32,7% de PO43-. Durante el periodo de investigación, la comunidad planctónica estuvo representada por las siguientes clases: Chlorophyceae, Euglenophyceae, Cyanobacteria, Cryptophyceae, Zygnemaphyceae, Chrysophyceae, y Dinophyceae; concurrentemente, el zooplancton registró bajas densidades y fue representado por los grupos Rotiferous, Copepod, y Cladocera. Los resultados permiten comprender el desempeño de las lagunas de pulimento en el tratamiento de efluentes sanitarios.

**Palabras clave:** calidad del agua; remoción de contaminantes; lagunas de estabilización; tratamiento de efluentes sanitarios

## Introduction

Waste stabilization ponds (WSPs) are widely used across the world as passive wastewater treatment for domestic effluents; WSPs are recommended to treat wastewater in small communities [1], [2]. Due to the simplicity of their design, low cost, minimal maintenance, and low-skilled operators, wsps have become one of the most popular biological wastewater treatment systems applied in many places around the globe [3 - 5]. wsp is natural technology installed in centralized or semi-centralized sewerage systems for treating domestic wastewater, septage and sludge, and animal and industrial wastes. It can be used as a secondary or tertiary treatment unit in a treatment plant individually or in a coupling manner [6], [7]. In developing countries, where sufficient land is available, using **WSPs** is the simplest and most sustainable municipal wastewater treatment method [8], [9]. One of the most important benefits of adopting wsps in the treatment process is their tolerance towards system shocks and significant fluctuations in wastewater characteristics, including flow rate, biochemical oxygen demand, total suspended solids, and ambient and inflow temperature [10]. In WSPs, algae and heterotrophic bacteria coexist for the treatment; such microorganisms control the effluent's treatment efficiency and quality [11], [12].

The main objective of this research was to study the behavior and evaluate the performance of a group of four polishing ponds during the post-treatment of sanitary sewage by monitoring variables such as DO, pH, alkalinity, BOD, COD, TKN, organic nitrogen, NH<sub>3</sub>, N-NO<sub>3</sub>, TP, PO<sub>4</sub><sup>3-</sup>, TSS and chlorophyll-*a*. In addition, the planktonic communities (phytoplankton and zooplankton) were also quantified.

## **Materials and Methods**

### **Study Site**

This research was carried out in Viçosa, State of Minas Gerais, Brazil (20°45'14" S, 42°52'54" W), at the Integrated Unit for Sewage Treatment and Effluent Use of the Violeira neighborhood, and is focused on the treatment of an average flow rate of 115 m<sup>3</sup>/d. The pre-treatment units included an up-flow anaerobic sludge blanket (UASB) reactor and a submerged aerated biofilter, both at full scale; four pilot scale polishing ponds, pre-fabricated in glass fiber, were used as post-treatment units, with an effective individual area of 16.3 m<sup>2</sup>, an average effective depth of 0.90 m and a length/width ratio equal to 2.0 (Fig. 1).

The research was carried out from February 2009 to June 2010, as operational malfunctioning prompted an interruption in November and December. In the course of the study, the pond group operated under two different hydraulic retention times (HRT), thence characterizing the two following operational periods: from February to October 2009 –Period I–: pond flow rate Q =  $3.5 \text{ m}^3/\text{d}$ , HRT = 4 days in each pond; January to June 2010 –Period II–: Q =  $2\text{m}^3/\text{d}$ , HRT = 7 days in each pond.

## Sampling and data analysis

The water's physical and chemical variables were measured in situ: temperature, with a bulb thermometer; dissolved oxygen, measured with an oximeter (Digimed, model DM-4); and pH,



Figure 1. Schematics of the experimental group of polishing ponds Source: The authors

measured by a pH meter (Digimed, model DM-21). The measurements were performed on three water levels: superficial (15 cm), medium (45 cm), and full-depth (90 cm).

The samplings were trialed during the two aforementioned operational periods via water collection from polishing ponds P1, P2, P3, and P4. At the Water Quality Control of Water and Sewage Division of the Universidade Federal de Viçosa (UFV), the following variables were monitored: BOD, COD, TSS, organic nitrogen, NH<sub>3</sub>, N-NO<sub>3</sub>, TP, PO<sub>4</sub><sup>3-</sup>, alkalinity and chlorophyll-*a*. In addition, the physical and chemical variables were monitored according to the recommendations of Standard Methods for the Examination of Water and Wastewater [13].

Water transparency was determined by lowering a 0.30 m white Secchi disk into the water until the white part of the disk disappeared; the depth of the disk in the water is the value of transparency [14], [15].

The data herein employed concerning precipitation (mm) and air temperature (°C) were granted by the meteorological station located at the UFV.

The phytoplankton composition was studied through samplings performed with a plankton net with 20  $\mu$ m mesh. The samples were collected with horizontally oriented drag force at a subsuperficial level. The samplings thus collected were separated into two groups, of which one was fixed with a formaldehyde solution of 4%, and the other was kept alive for further observation of its morphology – an ensemble of essential characteristics towards the act of taxonomic identification. These taxonomic inquiries used a Zeiss-branded microscope, model Axioskop, built-in phase contrast, epifluorescence, and a photographic camera.

The samplings for the study of phytoplankton density were carried out near the effluent tubes of each pond via a depth collector. The samples were preserved in a solution of acetic Lugol 5%, and phytoplankton density was gauged through the Sedgwick-Rafter chamber method of cell counting [13], making use of a Zeiss microscope, Axioskop model, whose sight was magnified four-hundredfold, of which it was a far-reaching objective lens.

The samples for analysis of the zooplankton were collected with a plankton net, whose mesh openings amounted to  $68 \mu$ m, contained in glass recipients, and preserved with formaldehyde 4%. Further taxonomic analysis and the quantification of organisms required using a stereoscopic microscope and an optic microscope magnified up to a thousandfold. The taxonomic analysis was performed at the level of large groups, using specialized literature concerning each group. Concurrently, the organisms were quantified using an acrylic cuvette of checkered background, and an individual/liter ratio expressed their population density.

## **Results an d Discussions**

### **Climate variables**

According to the Köppen climate classification, the region has a hot temperate climate with rainy summers and, conversely, dry, cold winters. The annual average of the rainfall index, relative humidity, and the yearly average temperature correspond to 1268.2 mm, 81%, and 20°C [16].

**Table 1.** During the study period, monthly pluviometric precipitation (Prec.) and average air temperature (Air T.) at the municipality of Viçosa-MG.

Month	Feb I	Mar I	Apr I	May I	Jun I	Jul I	Aug I	Sep I	Oct I
Prec. (mm)	170.2	273.4	29.9	0.8	38.2	1	13.2	96	123.5
Air T. (°C)	22.5	22.2	20	17.4	15.7	16.7	16.7	24.3	21
Month	Nov I	Dec I	Jan II	Feb II	Mar II	Apr II	May II	Jun II	
Prec. (mm)	137.5	393.5	57.9	45.5	184.8	28.1	35.4	0.9	
Air T. (°C)	22.9	22.4	23.2	23.3	22.2	19.6	17.5	14.1	

Source: The authors

Table 1 presents the values of monthly pluviometric precipitation and air temperature at the municipality of Viçosa between February of Period I and June of Period II.

## Physical and Chemical Variables of Water

#### Water transparency

The transparency of the water column displayed a trend of increasing values from P1 to P4. The polishing ponds P1, P2, P3, and P4 presented the following average values and respective standard deviations:  $40 \pm 9$ ,  $45 \pm 19$ ,  $48 \pm 16$ , and  $63 \pm 20$  cm. The maximum values obtained in P1 through P4 were 61.5, 88.5, 78.0, and 96.0 cm, and the minimum values were 27.0, 15.0, 24.0, and 28.5 cm, respectively.

The more transparent the water column, the better the light penetrates it. Therefore, photosynthetic activity increases, which culminates in oxygen production, thereby elevating pH, as it remains to be articulated in the following item.

#### Temperature, DO, and pH

Table 2 presents the maximum and minimum values measured, as well as the average values and standard deviations of the variables water temperature, **DO**, and pH for three different points concerning their positions in the water column:

Table 2. Minin	num, maximum, a	and average values,	, and standard	deviations for	T, DO,	and pH o	of the su	irface p	oint
(SP), medium	point (MP), and bo	ottom point (BP) foເ	und in the four	ponds during	researc	h. 🔨			

Variable			Pond 1			Pond 2	
Position		Min	Мах	Av ± SD	Min	Мах	Av ± SD
T (°C)	SP	19.2	28.2	24.0 ± 3.3	18.1	28.6	23.9 ± 3.0
	MP	18.7	27.0	23.0 ± 3.0	17.5	27.0	23.0 ± 3.0
	ВР	18.6	26.8	23.3 ± 3.0	17.3	26.0	22.7 ± 2.9
	SP	0.4	15	7.8 ± 4.5	2.1	18.1	10.1 ± 3.7
DO (ma/l)	MP	0.4	10.0	5.0 ± 2.0	1.2	11.0	5.0 ± 2.0
(119, 2)	ВР	0.0	4.0	1.4 ± 1.3	0.5	5.0	2.6 ± 1.2
рН	SP	7.0	9.1	7.7 ± 0.7	7.2	10.2	8.5 ± 0.8
	MP	6.9	8.5	$7.4 \pm 0.4$	6.9	9.1	8.0 ± 1.0
	ВР	6.5	7.9	7.1 ± 0.4	6.6	8.2	7.1 ± 0.4
Variable			Pond 3				
Variable			Pond 3	}		Pond 4	
Variable Position	$\mathbf{\mathbf{\nabla}}$	Min	Pond 3 Max	S Av ± SD	Min	Pond 4 Max	Av ± SD
Variable Position	SP	Min 18.5	Pond 3 Max 28.5	8 Av ± SD 24.2 ± 3.2	Min 18.5	Pond 4 Max 29.0	Av ± SD 24.2 ± 3.4
Variable Position T (°C)	SP MP	Min 18.5 17.9	Pond 3 Max 28.5 27.7	Av ± SD 24.2 ± 3.2 23.0 ± 3.0	Min 18.5 17.8	Pond 4 Max 29.0 27.5	Av ± SD 24.2 ± 3.4 23.0 ± 3.0
Variable Position T (°C)	SP MP BP	Min 18.5 17.9 17.6	Pond 3 Max 28.5 27.7 26.9	Av ± SD 24.2 ± 3.2 23.0 ± 3.0 22.7 ± 3.0	Min 18.5 17.8 17.5	Pond 4 Max 29.0 27.5 27.0	Av ± SD 24.2 ± 3.4 23.0 ± 3.0 23.0 ± 3.1
Variable Position T (°C)	SP MP BP SP	Min 18.5 17.9 17.6 1.4	Pond 3 Max 28.5 27.7 26.9 15.5	Av ± SD           24.2 ± 3.2           23.0 ± 3.0           22.7 ± 3.0           9.1 ± 3.6	Min 18.5 17.8 17.5 2.0	Pond 4 Max 29.0 27.5 27.0 21	Av ± SD 24.2 ± 3.4 23.0 ± 3.0 23.0 ± 3.1 8.8 ± 4.3
Variable Position T (°C) D0 (mg/L)	SP MP BP SP MP	Min 18.5 17.9 17.6 1.4 1.3	Pond 3 Max 28.5 27.7 26.9 15.5 9.8	Av ± SD           24.2 ± 3.2           23.0 ± 3.0           22.7 ± 3.0           9.1 ± 3.6           5.0 ± 2.0	Min 18.5 17.8 17.5 2.0 1.3	Pond 4 Max 29.0 27.5 27.0 21 9.8	Av ± SD           24.2 ± 3.4           23.0 ± 3.0           23.0 ± 3.1           8.8 ± 4.3           6.0 ± 2.0
Variable Position T (°C) D0 (mg/L)	SP MP BP SP MP BP	Min 18.5 17.9 17.6 1.4 1.3 0.8	Pond 3 Max 28.5 27.7 26.9 15.5 9.8 6.0	Av ± SD           24.2 ± 3.2           23.0 ± 3.0           22.7 ± 3.0           9.1 ± 3.6           5.0 ± 2.0           3.0 ± 1.5	Min 18.5 17.8 17.5 2.0 1.3 0.3	Pond 4 Max 29.0 27.5 27.0 21 9.8 8.3	Av ± SD           24.2 ± 3.4           23.0 ± 3.0           23.0 ± 3.1           8.8 ± 4.3           6.0 ± 2.0           3.8 ± 1.9
Variable Position T (°C) D0 (mg/L)	SP MP BP SP MP BP SP	Min 18.5 17.9 17.6 1.4 1.3 0.8 6.4	Pond 3 Max 28.5 27.7 26.9 15.5 9.8 6.0 10.2	Av ± SD           24.2 ± 3.2           23.0 ± 3.0           22.7 ± 3.0           9.1 ± 3.6           5.0 ± 2.0           3.0 ± 1.5           8.8 ± 1.0	Min 18.5 17.8 17.5 2.0 1.3 0.3 6.3	Pond 4 Max 29.0 27.5 27.0 21 9.8 8.3 11.0	Av ± SD           24.2 ± 3.4           23.0 ± 3.0           23.0 ± 3.1           8.8 ± 4.3           6.0 ± 2.0           3.8 ± 1.9           8.3 ± 1.4
Variable Position T (°C) DO (mg/L) pH	SP MP BP SP MP BP SP MP	Min 18.5 17.9 17.6 1.4 1.3 0.8 6.4 6.4	Pond 3 Max 28.5 27.7 26.9 15.5 9.8 6.0 10.2 9.4	Av ± SD           24.2 ± 3.2           23.0 ± 3.0           22.7 ± 3.0           9.1 ± 3.6           5.0 ± 2.0           3.0 ± 1.5           8.8 ± 1.0           8.0 ± 1.0	Min 18.5 17.8 17.5 2.0 1.3 0.3 6.3 6.3	Pond 4 Max 29.0 27.5 27.0 21 9.8 8.3 11.0 10.1	Av ± SD           24.2 ± 3.4           23.0 ± 3.0           23.0 ± 3.1           8.8 ± 4.3           6.0 ± 2.0           3.8 ± 1.9           8.3 ± 1.4           8.0 ± 1.0

Source: The authors

surface point (15 cm: **SP**), medium point (45 cm: **MP**) and bottom point (90 cm: **BP**) of the four ponds herein studied.

The water temperature in the ponds exhibited low variation between the treatment units during the study period (Table 2). In broad terms, the temperatures recorded were higher at the surface than at the bottom of the ponds.

During the research, the behavior of the water temperature followed the same dynamics of the environmental temperature presented in Table 1, representing both an increase and a decrease of these values due to the respective climatic periods of rain and drought in the municipality.

As expected, the highest dissolved oxygen concentrations were found on the surface of the ponds. The vertical **DO** profiles indicated decreasing levels in relation to the depth, as presented in Table 2. Pastich et al. [17] recorded high **DO** levels at the surface of a secondary maturation pond with a depth of 1.45 m and **HRT** of 6.8 days, with an average monthly concentration above 13.5 mg/L and low monthly average concentrations at the bottom, which amounted to 0.2 mg/L.

The behavior of the concentrations measured in the series of ponds corroborated the findings reported by Bastos et al. [18] in a study carried out in the same pond system, which observed, in general, a DO variation pattern with a tendency to increase as one progresses in the series of ponds and with more accentuated variations on the surface, resulting from the balance between photosynthesis and breathing activity (bacterial and algal), typical of daytime and night-time and along the depth of the pond.

Based on the pH data in the depth profile of the ponds over the research period, a variation pattern was observed with a surface reduction towards the bottom of the treatment units and a general increasing tendency as the pond series progresses.

The results revealed an alkaline condition in the water column, with a slight tendency to acidification at the bottom. In addition, a general pattern of pH variation similar to that of **DO** was observed, with an increasing trend ranging from Ponds 1 through 4; a similar condition was reported by Ouali et al. [19] in a series of three full-scale maturation ponds, with individual HRTs ranging from 2.46 to 2.85 days, located in Tunisia, which treated the effluent from a system of activated sludge.

In stabilization ponds, the photosynthesis carried out by microalgae increases the pH, which can reach values higher than 9.0 since there is high photosynthetic activity [20], a condition observed in the maximum values measured on the surface of the ponds.

#### Alkalinity

In general, decreased alkalinity was observed throughout the treatment process, a phenomenon reported by Pontes et al. [21] in the post-treatment of UASB reactor effluents through polishing ponds. The following average values and the standard deviations were calculated for the P1, P2, P3, and P4 ponds:  $135 \pm 53$ ,  $105 \pm 54$ ,  $84 \pm 40$ , and  $71 \pm$ 34 mg CaCO<sub>3</sub>/L, respectively. The minimum values measured in such ponds were 63, 30, 30, and 18 mg/L, recorded between February and May of the first year, and the maximum values were 272.2, 236.6, 182.2, and 134.0 mg CaCO<sub>3</sub>/L, measured in October of the same year, probably related to the precipitation of that month.

In stabilization ponds, several processes affect alkalinity and/or acidity (in turn, indirectly disturbing the pH value). The most critical processes are the biological removal of  $CO_2$  when photosynthetic consumption predominates over the production by bacteria or by desorption into the atmosphere and the desorption of NH<sub>3</sub>, equivalent to adding a strong acid [22]. In Bastos et al. [18] research on polishing ponds, reduced alkalinity was associated with high ammonia removal throughout the ponds.

#### Biochemical Oxygen Demand

Figure 2 presents the variations in BOD over the two study periods. The highest BOD values were generally registered in ponds P1 and P2, with gradual reduction towards P3 and P4.



Figure 2. BOD variation over the study period Source: The authors

During the first period of study, the decreased concentrations along the series of ponds may have been caused by the stabilization of organic matter by the bacterial community. For the second period, although a lower organic load was applied due to lower HRT, the increased BOD concentrations, especially in the second pond (Fig. 2), were associated with higher algal biomass proliferation; similar behavior was reported by Dias et al. [23] in the second maturation pond treating UASB reactor effluent.

The maximum BOD concentrations measured in ponds P1, P2, P3, and P4 during the research were, respectively, 65.3, 66.9, 48.6, and 37.5 mg/L; the minimum values reported in the ponds were 14, 16, 12, and 10 mg/L. The mean values and respective standard deviations were:  $30.1 \pm 14.1$ ,  $32.6 \pm 15.6$ ,  $23.9 \pm 11.6$ , and  $20.2 \pm 9.8$  mg/L. These concentrations are similar to those reported by Amengual-Morro et al. [24] in a maturation pond with an HRT of 21 days. Based on average concentrations in ponds 1 and 4, the average efficiency of BOD removal was 32.9%.

The performance of the ponds in BOD removal is an excellent complement to that achieved by the UASB reactor in association with the aerated biofilter, especially considering that Bastos et al. [25], in an operational control study of the same type of treatment system, reported that average BOD removal efficiency in UASB may reach values above 80%.

#### Chemical oxygen demand

Figure 3 presents the variation of COD concentrations during the study period.



Figure 3. Variation of COD concentrations during the research

Source: The authors

The variation in the values of this variable was similar to those exhibited by BOD. An increase was observed in the second pond and a decrease in the two following ponds. The maximum concentrations of COD recorded in the research were 306.7, 455.0, 198.8, and 206.3 mg/L for ponds P1, P2, P3, and P4, respectively, and the minimum values registered in the series of ponds were 63, 63, 98 and 67.5 mg/L.

The following values were obtained for the average concentration and standard deviation for each pond:  $162.6 \pm 75.3$  in pond P1;  $169.3 \pm 80.9$  in pond P2;  $150.1 \pm 35.6$  in pond P3; and  $119.5 \pm 40.2$  mg/L in P4. The average COD removal efficiency of 26.5% was obtained based on the average concentrations found in ponds 1 and 4. The relatively low COD removal in polishing ponds results from high algae concentration, predominant in this kind of treatment unit, representing organic matter [21], [23]. In a maturation pond with HRT of 21 days, after a two-year long monitoring, Amengual-Morro et al. [24] reported increased average concentrations of COD effluent with COD affluent, ranging from 343.7 to 375.1 mg/L.

#### Total suspended solids

In both study periods, an increasing trend was observed in TSS concentration, from P1 towards P2, which was also found by Dias et al. [23] in the second maturation pond in the post-treatment of UASB reactor effluent. At the same time, reduction was detected in P3 and P4 (Fig 4).



Figure 4. TSS variation during both study periods Source: The authors

Mean values and standard deviations for TSS, calculated in ponds P1, P2, P3, and P4, were, respectively,  $87.9 \pm 46.4$ ,  $101.0 \pm 51.2$ ,  $74.4 \pm 28.8$ , and  $62.4 \pm 29.1$  mg/L, which are close to the values reported by Pontes et al. [21] in post-treatment of **UASB** reactor effluent in polishing ponds, with **HRT** between 6 and 12 days, and water column depth of 45 cm. The minimum values recorded in each pond were 13, 17, 30, and 10 mg/L, and the maximum values were 180.0, 212.5, 118.0, and 112.3 mg/L. Based on the average concentrations of ponds 1 and 4, the average TSS removal efficiency during the experiment was 29.0%.

#### Nitrogen compounds

A gradual decrease in nitrogen compound concentrations was generally observed in the series of ponds during the study period, demonstrating the efficiency of polishing ponds in removing this macronutrient.

Figure 5 presents **TKN** variation in the series of ponds during the research period.



**Figure 5.** Variation of TKN concentration in the series of ponds during the study periods **Source:** The authors

In both periods, related behavior was observed in the series of ponds, with less variability in the second period, probably due to longer HRT. The highest concentrations of TKN during the experiment were 71.3, 51.0, 44.0, and 29.3 mg/L, respectively, found in ponds P1, P2, P3, and P4; the following means and standard deviation were calculated for the ponds:  $35.8 \pm 13.4$ ,  $26.2 \pm 10.9$ ,  $20.4 \pm 9.3$  and  $14.9 \pm 7.4$  mg/L; and the lowest concentrations recorded were 19, 12.3, 10.6 and 4.4 mg/L. The average concentrations calculated in ponds 1 and 2 were compatible with the ones reported by Pastich et al. [17] in a secondary maturation pond with an HRT of 6.8 days.

Based on average concentrations of pond 1 and pond 4, the TKN removal efficiency during the experiment was 58.4%, with better performance in the second pond, a condition also observed in the one exhibited by Dias et al. [23] in a treatment system composed of a UASB reactor followed by 2 maturation ponds and a granular filtration unit. Chiatti and von Sperling [26] evaluated the performance of polishing ponds in the removal of nitrogen in a system with 2 to 4 ponds in series, with depths of 0.4 and 0.8 m and HRT of 5.7 and 12.5 days; the authors observed that the series with 0.4 m depth (HRT = 5.74 d) were more efficient in total nitrogen removal (68%), while the series with 0.8 m (HRT = 12.48 d), reported a 59% average of total nitrogen removal, a value close to the average registered in the present research.

The mean values and standard deviation calculated for ammonia in ponds P1, P2, P3, and P4 were, respectively,  $21.7 \pm 8.8$ ,  $10.4 \pm 9.8$ ,  $5.3 \pm 7.1$ , and  $2.7 \pm 4.7$  mg/L; the maximum concentrations registered in the ponds were 43.4, 36.9, 27.9 and 14.7 mg/L; and the minimum measured values were 6.4 mg/L in pond P1; and 0 mg/L in ponds P2, P3 and P4. Based on the average concentrations of ponds 1 and 4, the standard ammonia removal efficiency during the experiment was 87.5%. Again, the best performance was observed in the second pond, which was also reported by Dias et al. [23]. The ammonia levels in the ponds were similar to those in facultative primary ponds at full scale, measured by Cruz [27], with concentrations ranging from 11.9 mg/L on the surface to 41.3 mg/L on the bottom.

Regarding organic nitrogen, the maximum concentrations measured in ponds P1, P2, P3, and P4 were, respectively, 35.0, 29.4, 42.6, and 24.1 mg/L; the respective mean values and standard deviations were:  $16.0 \pm 6.5$ ,  $15.9 \pm 6.4$ ,  $15.1 \pm 7.4$  and  $12.1 \pm 5.2$  mg/L; and the minimum concentrations registered were 7.3, 2.6, 8.2 and 4.4 mg/L. Therefore, based on the average concentrations of ponds 1 and 4, the standard organic nitrogen removal efficiency during the experiment was 24.4%.

The particulate organic nitrogen may be settled at the bottom of the pond or hydrolyzed to soluble organic nitrogen, which may be mineralized to ammonia. Other sedimentation processes of organic nitrogen can be auto-flocculation and microalgae sedimentation [22]. According to Arceivala [28], microalgae cell structure comprises 6 to 12% of nitrogen dry weight. von Sperling [20] estimated that the percentage of nitrogen removal through algae biomass loss with effluent is between 10 and 20%.

The maximum nitrate measured concentrations were 13.0, 9.7, 10.6, and 13.5 mg/L, respectively, in ponds P1, P2, P3, and P4; the following average values and the standard deviation were obtained for the ponds:  $5.3 \pm 3.1$ ,  $5.0 \pm 2.6$ ,  $5.6 \pm$ 2.6 and  $4.8 \pm 2.7$  mg/L; and the lowest concentration levels were 1.9, 2.5, 1.9 and 1.7 mg/L. Therefore, based on the average concentrations of ponds 1 and 4, the standard nitrate removal efficiency during the experiment was 9.4%.

The following mean values and standard deviations of nitrate concentrations were measured in the series of ponds during the first research period:  $6.7 \pm 2.5$ ,  $6.4 \pm 2.5$ ,  $6.7 \pm 2.2$ , and  $4.7 \pm 2.1$  mg/L, and in the second period:  $3.2 \pm 1.1$ ,  $2.8 \pm 0.3$ ,  $4.0 \pm$ 2.5 and 4.9  $\pm$  3.6 mg/L. In the first period, when receiving a greater effluent flow from the aerated biofilter, pond P1 also received higher nitrate levels, but there was a progressive decrease due to algae assimilation. However, P1 received lower nitrate levels in the second period due to longer HRT. Nevertheless, the concentrations presented a slight increase, probably due to favorable conditions for nitrification processes in the submerged aerated biofilter that transformed a higher amount of ammonia into nitrates when compared to the fraction assimilated by algae. The registered concentrations were usually superior to those measured by Dias et al. [23] in polishing ponds as they treated **UASB** reactor effluent.

#### Total phosphorus and orthophosphate

The variation of total phosphorus in the series of ponds is represented in Fig 6.



Figure 6. TP variation in the series of ponds Source: The authors

During the research, in ponds P1, P2, P3, and P4, the respective maximum concentrations measured for **TP** were 7.7, 7.7, 7.6, and 7.2 mg/L; the

following mean values and standard deviations were found:  $5.2 \pm 1.7$ ,  $4.8 \pm 1.8$ ,  $4.5 \pm 1.5$  and  $3.8 \pm 1.5$  mg/L; and the minimum measured concentrations were 2.8, 1.6, 2.5 and 1.8 mg/L. Based on the average concentrations of ponds 1 and 4, the **TP** removal efficiency detected during the experiment was 26.9%. The average calculated concentrations in pond 4 were similar to those reported by Pastich et al. [17], in a secondary maturation pond with an **HRT** of 6.8 days, in Pernambuco-Brazil.

The variation of orthophosphate concentrations in the polishing ponds is presented in Fig. 7.



Figure 7. Variation of orthophosphate in the series of ponds

Source: The authors

In ponds P1, P2, P3, and P4, the respective maximum concentrations of orthophosphate were 6.6, 6.5, 6.4, and 6.2 mg/L; the mean values and standard deviations for orthophosphate were  $3.5 \pm 1.5$ ,  $2.9 \pm 1.7$ ,  $2.8 \pm 1.2$  and  $2.3 \pm 1.2$  mg/L; the minimum concentrations registered were 1.9, 0.3, 1.3 and 0.5 mg/L. Based on the average concentrations of ponds 1 and 4, the orthophosphate removal efficiency during the experiment was 34.3%. The average concentrations calculated in the series of ponds were similar to the average monthly concentrations reported by Pastich et al. [17] while monitoring a secondary maturation pond.

While studying polishing ponds in Campina Grande – Brazil, Cavalcanti et al. [22] observed that higher phosphorus removals (60 to 80%) are only reached in shallow ponds ( $h \le 0.65$  m), with at least 9 pH units. In general, the rate of

orthophosphate removal was slightly higher than that of total phosphorus removal, following the data reported by Assunção and von Sperling [29] in a series of three polishing ponds treating UASB reactor effluent, with individuals HRT between 1.5 and 4.3 days.

## **Biological Variables**

# Chlorophyll-a and phytoplankton community

The variation of Chlorophyll-a concentration in the series of ponds presented a decreasing tendency in P1 towards P4 during the study, and the highest values were registered in pond P2. The maximum concentrations recorded were 554.5, 453.9, 465.8, and 385.0  $\mu$ g/L, respectively, in ponds P1, P2, P3, and P4; the mean values and standard deviations were: 200.3 ± 150.5, 222.2 ± 123.5, 149.8 ± 115.4 and 99.8 ± 120.6  $\mu$ g/L; and the minimum measured concentrations were 0, 39.5, 4.5 and 0  $\mu$ g/L.

During the research, individuals from seven classes were observed: Chlorophyceae, Euglenophyceae, Cyanophyceae, Cryptophyceae, Zygnemaphyceae, Chrysophyceae, and Dinophyceae. The first four were numerically representative. The highest densities observed in the pond correspond to individuals from class Chlorophyceaea, as shown in Table 3.

During the research, the phytoplankton community was generally represented by the following classes: Chlorophyceae (51.5%), Euglenophyceae (20.4%), Cyanobacteria (17.5%), Cryptophyceae (5.8%), Zygnemaphyceae (1.9%), Chrysophyceae (1.9%) and Dinophyceae (1.0%).

Organisms from class Chlorophyceae are opportunistic microalgae that develop well under extreme conditions, especially in waters with a high level of eutrophication. This class was predominant in polishing ponds in Vitória, Espírito Santo-Brazil [27]; in a polishing pond with HRT of 10.5 days in Venda Nova do Imigrante, Espírito Santo-Brazil [30] and in a primary facultative pond in Barbalha, in the state of Ceará-Brazil [31].

During the study period, the class Euglenophyceae exhibited the highest densities in ponds P1

Class	Pond	Min	Мах	Av ± SD	Pond	Min	Мах	Av ± SD
Chlevenhusses	P1	6861	146994	33000 ± 32964	P2	5182	90947	36859 ± 26256
Chlorophyceae	P3	1714	96452	27803 ± 25706	P4	2060	129023	27003 ± 33574
Fueles enhances	P1	241	24633	6924 ± 6875	P2	273	17570	5444 ± 5901
Euglenophyceae	P3	98	9672	2272 ± 2626	P4	29	9625	1572 ± 2310
Granankuraa	P1	85	23021	3345 ± 5169	P2	0	9254	2540 ± 2832
Суапорпусеае	P3	0	10591	3228 ± 3356	P4	310	15260	3805 ± 3843
Countershires	P1	0	14814	2074 ± 4018	P2	0	14555	1735 ± 3610
стурторпусеае	Р3	0	5885	1207 ± 1997	P4	0	8483	1091 ± 1904

**Table 3.** Minimum values (Min), maximum values (Max), average values (Av), and standard deviation (SD), in cell/mL, for the numerically representative phytoplankton classes in the four ponds during the research

Source: The authors

and P2 and much lower concentrations when compared to the class Chlorophyceae, with a maximum value of 4633 cells/mL. An opposite behavior was observed in Euglenophyceae's growth if compared to Chlorophyceae's growth in the series of ponds. The predominant classes in the primary facultative pond and the maturation pond of the wastewater treatment plant of Trindade in the State of Goiás-Brazil were Chlorophyceae, Euglenophyceae, and Cyanophyceae [32], with HRT of 4.8 and 2.5 days, respectively.

The highest densities of individuals from class Cyanophyceae were registered in pond P1 in February of Period II and in August of Period 0 in P4. No organisms from class Cyanophyceae were found either in samplings from February of Period I in P3 or in August of Period I, March, and May of Period II in P2.

The class Cryptophyceae exhibited low-density values during the sampling period, ranging between the minimum of 23 cells/mL in P3 (February of Period I) and the maximum of 14814 cells/ mL in P1. In addition, there was an evident time separation, with low densities in the first period of the experiment and higher values during the second.

While investigating the effect of HRT and surface loading rate on the composition of phytoplankton community in polishing ponds on a pilot scale, von Sperling and Oliveira [33] observed the dominance of classes Chlorophyceae and Euglenophyceae. In the present study, statistical results pointed to a significant difference in the density of class Cryptophyceae during the sampling period. Furthermore, low density coincided with the period when the system was operated with shorter HRT (4 days), revealing changes in the planktonic community.

The classes that exhibited the lowest densities were Dinophyceae (38 to 506 cells/mL) and Zignemaphyceae (37 to 1502 cells/mL), and organisms from class Dinophyceae were only found in three sampling collections: October of Period I and January and May of Period II.

#### Zooplankton community

In general terms, the zooplankton found in the series of ponds presented low density, with total values of 460 org/mL in P1, 2506 org/mL in P2, 1149 org/mL in P3 and 597 org/mL in P4.In the studied system, regarding total densities, the group Rotifer exhibited the highest densities in ponds P1, P2, P3, and P4, with 195.9, 2172.0, 781.9, and 406.9 organisms/mL; the group Cladoceran revealed total densities of 82.8, 134.6, 81.8 and 37.0 organisms/mL; and the densities of group Copepod were 31.3, 130.0, 216.1 and 75.3 organisms/mL; the total densities of mosquito larvae were 149.5, 70.1, 72.7 and 83.3 organisms/mL.

The Zooplankton community presented time variation during the study period, with the disappearance of some organisms. In P1, zooplankton was not detected in 55% of the samples. In August of Period I, there was a peak in P2, mainly due to Rotifer's high density (1049 org/mL).

Several studies have demonstrated the sensitivity of the Copepod community to water quality changes [34], [35], which helps to explain the lower densities of these organisms in P1 (where higher organic loads were applied).

Moscoso et al. [36] observed intense proliferation of ciliates, rotifers, copepods, and cladocerans in a series of stabilization ponds in San Juan de Miraflores-Lima, Peru. In the city of Deli, India, Nandini [35] registered rotifers, cladocerans, and copepod populations in two systems of stabilization ponds. Each was distributed in four ponds with varying depths but with individual areas of 0.75 hectares. Ouali et al. [19] also registered Rotifer and Cladoceran populations in three maturation ponds in a series in Tunisia.

## Conclusions

The system of polishing ponds studied was efficient in reducing particulate material and organic matter, which resulted in effluents with average concentrations of TSS, BOD, and COD of 62.4, 20.2, and 119.5 mg/L, respectively, with average removal efficiencies of 29.0, 32.9 and 26.5% for such parameters.

The ponds performed well in the removal of nitrogen compounds, with average effluent concentrations in the fourth polishing pond of 14.9, 2.7, 12.1, and 4.8 mg/L, respectively, for NTK, NH<sub>3</sub>, organic nitrogen, and nitrates, which correspond to removal efficiencies of 58.4, 87.5, 24.4 and 9.4%. The average effluent concentrations for total phosphorus and orthophosphate were 3.8 and 2.3 mg/L, respectively, with average efficiencies of 26.9 and 34.3%.

The total cell density of phytoplankton in the series of ponds presented a wide range of variation, with four numerically representative classes: Chlorophyceae, Euglenophyceae, Cyanophyceae, and Cryptophyceae, whose average densities of 27003, 1572, 3805 and 1091 cells/mL were found in the final effluent.

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