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The interaction of vortical flows with red cells in venous valve mimics

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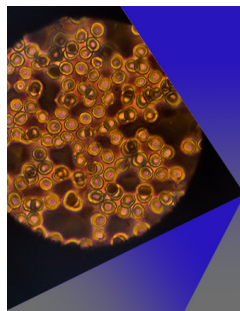
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ABSTRACT

The motion of cells orthogonal to the direction of main flow is of importance in natural and engineered systems. The lateral movement of red blood cells (RBCs) distal to sudden expansion is considered to influence the formation and progression of thrombosis in venous valves, aortic aneurysms, and blood-circulating devices and is also a determining parameter for cell separation applications in flow-focusing microfluidic devices. Although it is known that the unique geometry of venous valves alters the blood flow patterns and cell distribution in venous valve sinuses, the interactions between fluid flow and RBCs have not been elucidated. Here, using a dilute cell suspension in an *in vitro* microfluidic model of a venous valve, we quantified the spatial distribution of RBCs by microscopy and image analysis, and using micro-particle image velocimetry and 3D computational fluid dynamics simulations, we analyzed the complex flow patterns. The results show that the local hematocrit in the valve pockets is spatially heterogeneous and is significantly different from the feed hematocrit. Above a threshold shear rate, the inertial separation of streamlines and lift forces contribute to an uneven distribution of RBCs in the vortices, the entrapment of RBCs in the vortices, and non-monotonic wall shear stresses in the valve pockets. Our experimental and computational characterization provides insights into the complex interactions between fluid flow, RBC distribution, and wall shear rates in venous valve mimics, which is of relevance to understanding the pathophysiology of thrombosis and improving cell separation efficiency.

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INTRODUCTION

Red blood cells (RBCs) or erythrocytes are the most abundant cells in blood with 5×10^9 cells/ml accounting for 40%–50% (known as hematocrit or HCT) by volume in a healthy individual. RBCs are highly deformable, and the unique deformability characteristics of a RBC are key in the fluid and mass transport processes in the vasculature.¹ Although RBCs have mostly been appreciated in the context of tissue oxygenation, ischemia, and vaso-occlusion, several epidemiological studies have detected varying associations between hematocrit levels and thrombosis.^{2–5} The RBC composition in the blood clots depends on local flow rates—venous thrombi, which are typically associated with low flow conditions or blood stasis, are richer in red cells than arterial thrombi, which are typically associated with high flow conditions.⁶ In addition, flow-induced hemolysis and device-related thrombosis are causal to complications associated with left ventricular assist devices (LVADs) and extracorporeal membrane oxygenators (ECMOs).⁷ Therefore, it is important to understand how blood flow dictates local RBC distribution.

Numerous and excellent experimental and computational studies have investigated the role of RBC concentration, deformability, shape, and hydrodynamic interactions, mostly in straight, stenosed, or bifurcating channels in the context of hemostasis or thrombosis.^{8–13} However, relatively little effort has been expended in understanding blood flows inside a cavity or a sudden expansion, which is of relevance to flows in artificial devices (LVADs and ECMOs) and physiological systems (aortic aneurysms and venous valves). Of interest, a growing body of evidence points to the important contribution of RBCs in the pathophysiology of venous thrombosis.^{14,15} Venous thrombosis (VT) originates in the sinuses of venous valves, which are layered flaps in peripheral veins that prevent the backflow of blood.¹⁶ The venous valve sinuses are regions of low flow, and flow stasis in the valve sinus is long considered to be a major factor triggering venous thrombosis.^{17–19} The presence of a large cavity immediately distal to sudden expansion gives rise to unique flow patterns in the venous valve sinuses as observed in *ex vivo* fixed valves,²⁰ *in vivo* ultrasound studies,²¹ and

in vitro biomimetic valves.^{22,23} Experimental flow visualization studies show that these unique flow patterns due to sudden expansion result in differential RBC distribution in the distal pockets vs the center of the channel.^{24,25} However, there is insufficient information how these flow patterns determine RBC transport and local hematocrit distribution in the venous valve sinuses. This information on the interaction of recirculating flows with red cells can also be valuable for the growing interest in predicting thrombotic risks from patient-specific flow patterns determined by the vessel geometry.

In this work, we seek to determine experimentally the effect of venous valve hydrodynamics on local RBC distribution. Using microfluidics, micro-particle image velocimetry (μ PIV), computational fluid dynamics (CFD), and microscopy, we resolve the impact of local velocity fields and shear rates on RBC distributions in venous valve mimics. We use a dilute suspension of RBCs so that the individual cells could be discriminated without overcrowding, minimizing the confinement effects in the scale-down microfluidic model, and the role of fluid–cell interactions in RBC distribution may be studied without the confounding effects of cell–cell interactions that are prominent at physiological hematocrit levels.²⁶ From the images of RBC distribution at various flow rates,

we demonstrate that the local RBC concentrations in the valve sinuses are dramatically different from bulk flow due to vortical flows in the sudden expansion. We also determine the minimum shear rates necessary to drive the RBCs into the vortex and show that entrapment leads to a long residence time.

METHODS

The experimental system consisted of an infusion pump for positive pressure driven flow through the microfluidic chip, which was mounted on a microscope objective for the visualization of both RBC distribution and μ PIV (Fig. 1). The dimensions of the microfluidic channels are designed to mimic venous valves that are partially closed, leading to sudden expansion, and the channel Reynolds number (Re) was matched with what has been reported previously in *in vivo* flows.^{20,27}

Microfluidic device

A microfluidic device was designed to mimic venous valves using CAD software (AutoCAD, San Rafael, CA).⁵⁰ To simulate the sudden expansion in the valves, the main channel suddenly expands from a narrow constriction of 30 to 300 μm . The walls of

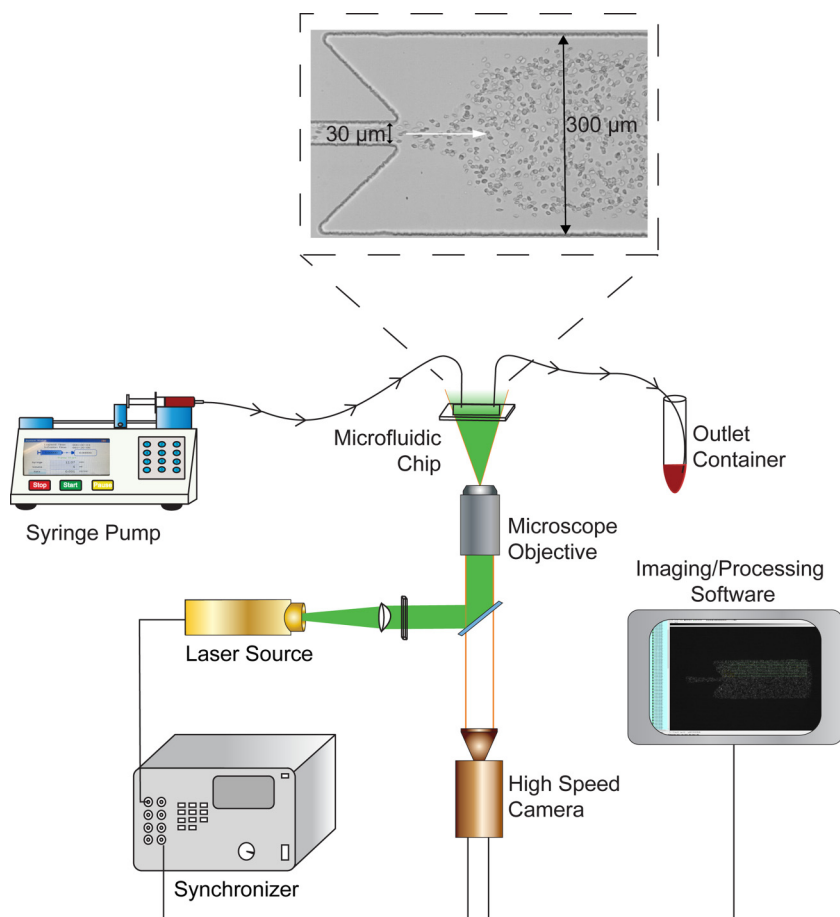


FIG. 1. Schematic of the full experimental setup used for RBC distribution and μ PIV measurements. The cutout window shows the microfluidic geometry, including the 30–300 μm with a valve angle of 135°. The white arrow indicates the direction of flow. RBC or bead suspension was perfused through the device at constant pressure using a syringe pump and analyzed either by microscopy or by μ PIV, respectively. When acquiring bright field images for RBC distribution measurements, the laser and synchronizer were not used; the high-speed camera took direct images of the flow device.

the valve pockets are angled at 135° relative to the direction of flow. The design was printed on a bright field mask, and using this mask, a silicon wafer was fabricated by soft lithography. A wafer was coated with SU-8 2035 to create a mold with a height of 35 μm . The mold was silanized with 95%–100% trichlorosilane (Gelest, Morrisville, PA) to preserve the design and prevent adhesion to the elastomer. The silicone base (Dow Corning, Midland, MI) was mixed with the curing agent at a ratio of 10:1 by weight to create polydimethylsiloxane (PDMS, Dow Corning, Midland, MI). The solution was poured onto the wafer and cured for 2.25 h at 90 °C (Precision Oven, Model 658, Thermo Scientific). The required design was cut and the inlet and outlet holes were punched using a 1-mm biopsy punch (Miltext, York, PA). The PDMS designs were sonicated in a bath sonicator (Model 75HT, LabX) for 10 min at room temperature in 35% ethanol solution to remove any debris. They were then rinsed in DI water and left to dry for 1 h at 90 °C. After cooling, PDMS and the microscope glass slide (Fisher Scientific, Waltham, MA) were activated by exposure to oxygen plasma (Basic Plasma Cleaner, Model PDC-32G, Harrick Plasma). These surfaces were immediately pushed together firmly to create an airtight seal. The chips were left to cure for 2 h at 90 °C to make the binding irreversible. The chips were prepared 24 h before the experiment to provide enough time for hydrophilic decay of PDMS to baseline levels.

Cell preparation

Venous blood was freshly drawn from healthy volunteers after signing an informed consent and obtaining written ethics approval in accordance with the Institutional Review Board (IRB) protocol (IRB F16134, Office of Research, SJSU). The red blood cells (RBCs) were separated from whole blood by spinning at 250 RCF with 7 acceleration and no breaks for 25 min at 22 °C (Eppendorf, Hamburg, Germany). The top plasma layer and the middle buffy coat were discarded. A dilute RBC suspension at a desired hematocrit concentration was prepared by diluting the appropriate volume of RBCs in a modified PBS buffer at physiological pH. This modified PBS buffer consisted of 1% dextrose and 0.5% BSA to prevent fast settling and nonspecific aggregation, respectively; and this was filtered using a 0.22-micron filter (Millipore PES Membrane) to remove dust and reduce clogging of the channel. The chip was primed right before running the experiment with 0.1% F-127 (MilliporeSigma, Burlington, MA) diluted in PBS. Once the buffer and PDMS device were prepared, the diluted RBC suspension was mixed gently with a pipette and drawn into a syringe using a 21 G needle, a 750 μm ID tube to keep the seal tight and connect the needle to the inlet of the chip. Flow rates of 0.01, 0.05, 0.1, 0.2, 0.3, and 0.4 ml/min corresponding to the Reynolds numbers of 0.6, 3, 6, 12, 18, and 24, respectively, were used. All flow conditions were allowed to stabilize for 1 min before commencing the video recording.

Image acquisition

The RBC movement within the microfluidic channel was monitored with a 20 \times objective/aperture 7 (Leica Dmi8 and LAS-X). Microscope settings also included 255 brightness intensity. The images were captured using a high-speed camera (Phantom

VEO 410-L). The images were captured at 10 068 fps at a resolution of 1024 \times 512 with an exposure time of 1 μs . The RBC distribution was averaged from 100 ms duration of frames for lower Re and from 10 ms duration of frames for higher Re.

Image analysis

The images were analyzed offline using ImagePro 10 (Media Cybernetics, Rockville, MD). Using inbuilt background subtraction and contrast enhancement algorithms, the RBCs were isolated from the background based on an intensity histogram. Using a custom MATLAB code, each image was binarized. To quantify RBC distribution from the binarized images, the images were divided into zones using grids 15.19 \times 20.21 μm^2 . The percentage of white pixels was calculated for each grid; these numbers were the 2D area density at that grid location. These values corresponded to specific HCT values on the calibration curve relating area density to HCT.

μPIV experiments and analysis

μPIV image acquisition

To trace fluid streamlines, we used micro-Particle Image Velocimetry (μPIV). Red fluorescent beads of 1 μm (Dyed Red Aqueous trace fluid streamlines Fluorescent Particles, Thermo Scientific) were used as tracer particles. The stock solution was sonicated and vortexed before preparing a 1:20 dilution of the working solution, corresponding to a final concentration of 0.05% w/v. The optical system was coupled with Nd: YAG double-pulse (YAG200-15-QTL) with an emission wavelength of 532 nm and a synchronizer (LaserPulse Model 610036). This μPIV system was controlled using Insight 4G software (TSI Incorporated, Shoreview, MN). The images were obtained at a repetition rate between 2500 and 18 754 Hz to obtain optimal images for further analysis.

During acquisition, an *in situ* point processing was performed as a quick check to ensure that the PIV image pair obtained had suitable Δt and adequate spot size. It was also necessary to verify that the particle displacement lies within the interrogation region for one spot analysis by using the quick point processing tool. This analysis compares the signal-to-noise ratio to the threshold.

μPIV image analysis

The detailed image analysis was performed offline, and it consisted of three steps: (1) Pre-processing: The quality of the image was improved by using image subtraction and removing noise using a minimum intensity operator; (2) Processing: A static mask was drawn as a boundary around the walls of the channel. The correlation between two spots was obtained using Fast Fourier Transform, and the image match within a displacement range was provided using the correlation function for each pixel. The peaks in the correlation values were obtained using the Gaussian peak function to determine the displacement of the particles within the spot pair. This information, along with Δt between the two frames, was used to calculate the vector direction and magnitude; (3) Post-processing: The data obtained were further processed to remove sporadic vectors using the vector validation process. The validation pipeline involved the use of a reference vector in global validation, local validation, and vector conditioning. The reference

vector was calculated using the median of the 5×5 neighborhood vectors. The difference between the vector velocities was used as tolerance to remove invalid vectors. Then, the removed vectors were replaced with the local median values. Global vector validation applied a range filter to the whole vector field, which was then used to eliminate vectors with a velocity magnitude outside the user-defined range. The spaces in the vector field due to failed SNR were filled using the local mean of the 3×3 neighborhood. Vector smoothing was performed by replacing them with a Gaussian-weighted mean of the vectors in a 3×3 neighborhood. Computational fluid dynamic software was used for visualization and presentation of the data (Tecplot 360, Bellevue, WA).

Computational fluid dynamics

A computational fluid dynamics study was performed to simulate flow behavior in the channels using COMSOL Multiphysics software (Version 5.5). The simulations were performed in 3D geometry. The material properties of water were used for the simulations. Since the bead suspension was dilute (0.05%), it was assumed that these particles do not impact the streamlines. No slip condition was applied at the walls, and normal flow and suppressed backflow were set at the outlet. Automatic meshing yielded a total of 589 105 domain elements, 78 386 boundary elements, and 2901 edge elements. Water was perfused through the channel at the flow rates corresponding to the experimental values, and the Navier–Stokes equations were solved with flow boundary conditions. The local velocities and streamlines were computed to compare with the experimental results.

Statistical analysis

All experiments were performed at least three independent times on different days, and each experiment was performed using at least two different channels. RBC experiments were performed on different days with blood drawn from three to six different donors. The data were analyzed using the Mann–Whitney U test to establish significance. A $P < 0.05$ was deemed as a statistically significant difference.

RESULTS AND DISCUSSION

Visualization of local hematocrit in the channel

We perfused a 5% hematocrit (HCT) suspension through the valve at the channel Reynolds (Re) numbers of 0.6, 3, 6, 12, 18, and 24. The Re was calculated as $Re = Wv\rho/\mu$, where W is the channel height, v is the average velocity, and ρ and μ are the fluid density and dynamic viscosity, respectively. For a femoral vein of ~ 6 mm diameter, these Re numbers correspond to a wall shear rate of ~ 10 – 400 s^{-1} . The diameters of, and flow velocities in, the femoral and saphenous veins are of the order of 0.5–12 mm and 1–40 cm/s, respectively, and varies depending on the posture.^{20,27,28} Therefore, the Re in venous flow is of the order of 1–75, which is comparable to our experimental system. RBC distributions, visualized by brightfield microscopy, are shown in Fig. S1 in the [supplementary material](#). In order to quantify these qualitative observations from the images, we prepared a calibration curve to map the image data to hematocrit estimations. To this end, in a separate experiment, for various hematocrits ranging

between 0.1% and 20%, images of slowly moving RBCs were collected, and the intensity of the RBCs over the background was quantified. As shown in Fig. S2 in the [supplementary material](#), the pixel intensities linearly correlated between 0.1% and 15% and saturated as the hematocrit was increased beyond 15%. Based on this calibration, relating 2D pixel densities to 3D hematocrit values, we computed the local hematocrit throughout the channel at different Re numbers (Fig. 2), with the color scale shown on the right corresponding to the hematocrit value obtained from the calibration curve.

Figure 2 shows local hematocrit distributions that result from flowing a feed solution of 5% hematocrit through the venous valve with the Re numbers of 0.6, 3, 6, 12, 18, and 24. At low Re ($Re = 0.6, 3,$ and 6), hematocrit distribution was uniform throughout most of the channel at a value comparable to that of feed hematocrit [Figs. 2(a)–2(c)]. The actual values vary slightly on either side of 5% because the suspension is dilute and the averaging process during image analysis. The asymmetry observed particularly at $Re = 0.6$ is due to the inevitable settling of RBCs at near zero flow rates. At these Re numbers ($Re = 0.6, 3,$ and 6), no RBCs were seen in the valve sinus regions, which are the angled wing regions

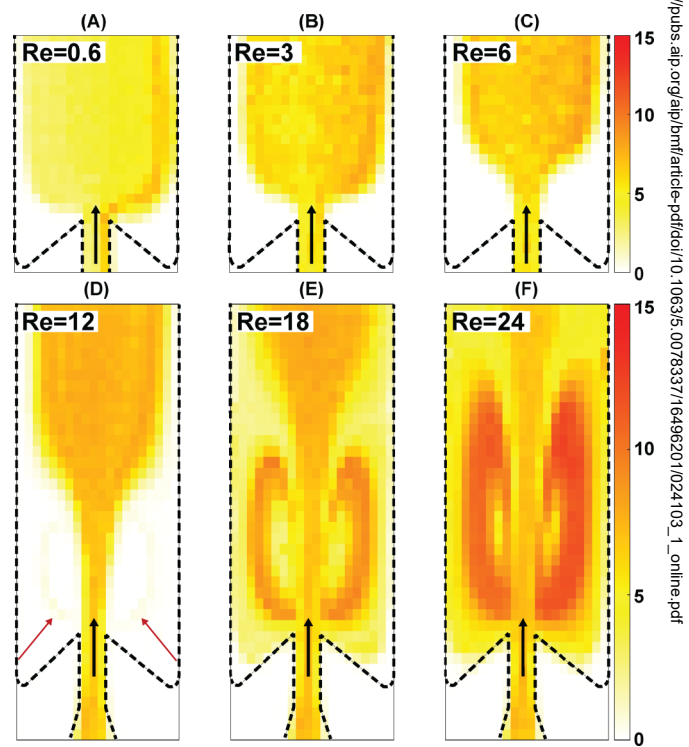


FIG. 2. Heat maps showing the RBC distribution for different Reynolds numbers as indicated (a)–(f). The black arrows indicate the direction of flow in the channel marked with dashed lines at the indicated Reynolds numbers. The color scale on the right depicts the hematocrit obtained by matching RBC distributions shown in Fig. S1 in the [supplementary material](#), with the calibration curve shown in Fig. S2 in the [supplementary material](#). The arrows at $Re = 12$ highlight the presence of RBCs in vortices.

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behind the sudden expansion. However, as the flow rate was increased, at $Re = 12$, an RBC vortex on either side of the main flow appeared. The vortex comprised less than ten cells on each side of the channel entering the valve sinus regions from the main channel flow. These vortices correspond to a local hematocrit of $<2\%$. At $Re = 18$ and 24 , the RBC density increased in the vortex regions significantly compared with that of $Re = 12$. We observed that the local hematocrit levels in the vortices increased more than the feed hematocrit levels to $\sim 8\%$ at $Re = 18$, which increased to as high a value as closer to 15% at $Re = 24$.

RBC distribution profiles

To compare the RBC distributions at different Re numbers and different locations along the channel, we quantified the RBC distribution along the cross sections at three locations, at the entrance ($140\ \mu\text{m}$ before the constriction), at the expansion ($70\ \mu\text{m}$ after the constriction), and at the exit ($380\ \mu\text{m}$ after the constriction) (Fig. 3). At the *entrance* to the channel, the positions of the RBCs were similar at all Re numbers, with the maximum hematocrit of $\sim 6\%$ right in the middle of the channel. At the *exit*, the positions of the RBCs at all Re numbers, except the highest ($Re = 18$ and 24), show similar plateau shapes. This represents a fully developed flow at the exit that has an even distribution of RBCs across the width of the channel. At $Re = 18$ and 24 , the distributions differ from those at lower Re by remaining flat through the channel cross section, indicating flow that is still developing at the exit location.

The RBC distributions near the *expansion* of the channel (blue line) capture the transition in distributions that occur with the increase in Re . We observe that at a low Re of 0.6 , nearing creeping flows, the RBC distribution is fully developed $\sim 50\ \mu\text{m}$ after exiting the constriction, resulting in a distribution at the expansion that matches that of exit [Fig. 3(b)]. As the Re is increased to 6 and 12 , the RBC distribution width at the expansion resembles that of the entry more than the exit (narrow distribution at the entry vs wide distribution at the exit). At these Re numbers (6 and 12), the flow is no more creeping, and the effects of the expansion are carried further downstream, and hence, the cells are concentrated in a $\sim 100\ \mu\text{m}$ region at the center of the channel.

As the Re is increased further to 18 and 24 , we observe a sudden increase in the RBC concentrations in the expansion region (blue line). Unlike at $Re = 0.6$ or 12 where RBC distribution along the cross section was uniform, the distributions at $Re = 18$ and 24 showed non-uniform patterns. At $Re = 18$, the distributions ranged between 3% and 9% , while at $Re = 24$, the maximum hematocrit was $\sim 12\%$, which was almost double the hematocrit at the center of the channel. The local decrease and increase in hematocrit levels are well visualized in the heatmap distributions shown in Figs. 2(e) and 2(g).

Feed or bulk hematocrit is operationally used to define the effects of RBCs on the formation and properties of venous thrombi.¹⁴ Emerging evidence shows that RBCs directly modulate thrombosis through several mechanisms, including thrombin generation, platelet activation, and clot strength.¹⁵ Our results from Figs. 2 and 3 show that the valve hematocrit is higher than the bulk

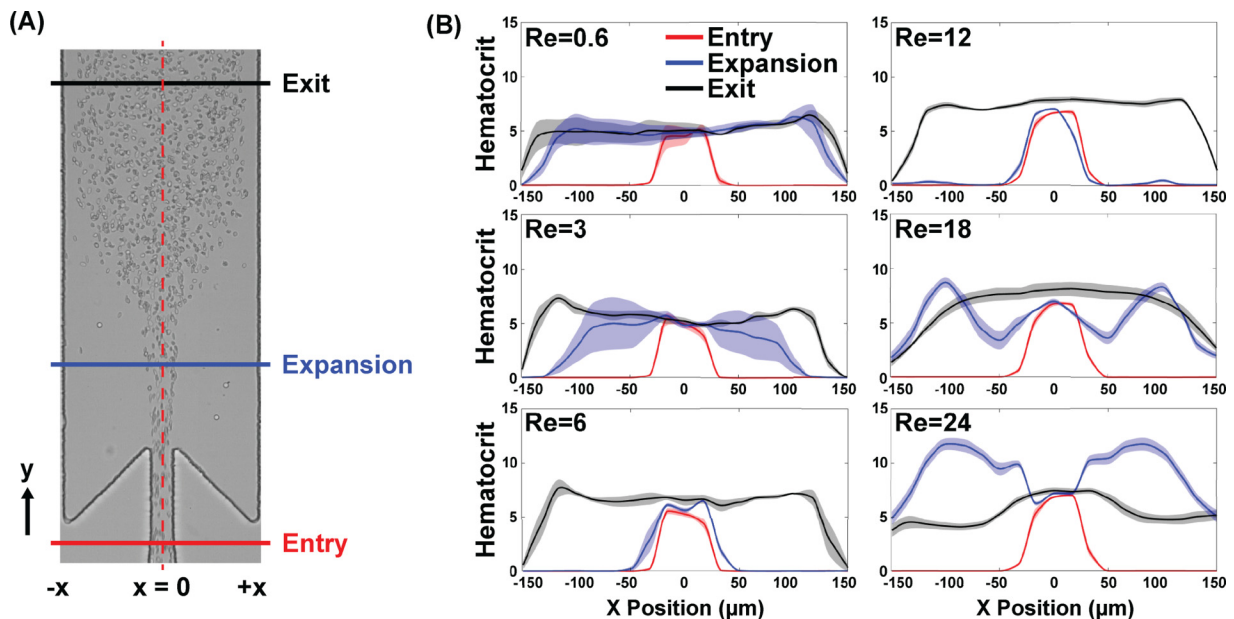


FIG. 3. Hematocrit profiles along the microchannel. (a) Hematocrit distributions across the channel cross section were estimated at the indicated locations entry ($-140\ \mu\text{m}$ from constriction), expansion ($+70\ \mu\text{m}$ from constriction), and exit locations ($+380\ \mu\text{m}$ from constriction). (b) Local hematocrit was estimated at these locations for a feed of 5% hematocrit and represented as mean \pm SEM ($n = 3-6$).

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hematocrit. It is likely that the difference in hematocrit between the vortex and the bulk flow observed in dilute suspension in this work will be more pronounced at physiological levels: for instance, a feed hematocrit of 25% has a greater RBC concentration than the feed near the channel walls in a sudden expansion when compared with a feed of 5% hematocrit.^{25,29} Therefore, local hematocrit rather than bulk hematocrit should be taken into consideration while evaluating the effects of RBCs on venous thrombosis.

Entrapment of RBCs in vortices

As described in Figs. 2 and 3, RBC vortices were observed at $Re = 12, 18,$ and 24 . We observed from high speed video microscopy (Movie M1 in the supplementary material) that, at a steady state, the RBCs remained within the vortex region for the entire duration of the analysis (2–5 s, at a frame rate of 10 068 fps). As a representative analysis of vortex dynamics, we tracked the position and velocities of individual RBCs in the vortex at $Re = 18$. Figure 4(a) shows the position and velocity magnitudes of cells in the outer, middle, and inner limit cycles of the vortex region. These trajectories and instantaneous RBC velocities were obtained by frame-by-frame tracking of the centroid of single cells. As Fig. 4(a) shows, at the bottom of the vortex, as the cells travel with the jetting stream, the velocity is as high as $1000 \mu\text{m/s}$, and at the top of the vortex and closer to the wall, the velocities drop to as low as $10\text{--}20 \mu\text{m/s}$ in the direction opposite to the main flow. Between these velocity changes, the RBCs decelerate when they travel toward the wall and accelerate when they join the forward flow. The near zero velocities of the RBCs close to the wall may have consequences in modulating the interaction and adhesion to the endothelial lining of the blood vessels. This analysis shows that RBCs, once entrapped in the vortices, follow their limit cycles with a long residence time. The average hematocrit in the vortices increased linearly and rapidly with increasing the Re beyond $Re = 12$ [Fig. 4(b)]. We also quantified the total RBCs that are trapped in the vortices by summing up over the entire vortex region at each Re . At a Re below 6, this value was nearly zero but increased rapidly at a higher

Re due to an increase in both the hematocrit and the size of the vortex: at $Re = 12, 18,$ and 24 , the total RBCs were $10.2 \pm 5.3, 75.1 \pm 12.1,$ and 140.1 ± 5.3 , respectively.

Development of microflows and vortices with increase in Re

To understand the RBC distribution in vortex flows at $Re = 12, 18,$ and 24 , and an anomalous increase in hematocrit levels at $Re = 18$ and 24 , we sought to analyze the flow patterns in the channels that drive the RBC movement. Fluorescent beads were used to track the flow patterns independent of and distinct from RBC distribution patterns. μPIV was used to obtain the velocity profiles from bead locations captured using high speed video microscopy. We visualized and quantified streamlines through the channels at $Re = 3, 6, 12,$ and 18 , noting that no RBC vortices were seen at $Re = 3$ and 6 . In Fig. 5, we show the streamlines and vorticity computed from μPIV analysis at these four Re numbers. At a low Re ($Re = 3$), a small amount of backflow was detected in the valve pockets (velocity on the order of 10^{-3} m/s compared with 10^{-2} m/s in the main channel). As the Re increased to $6, 12,$ and 18 , we observed an increase in the separation of the streamlines, and more backflow into the valve pockets was seen.

To quantify the location of flow separation leading to backflows, we computed the vorticity throughout the channel from the local velocity vectors estimated by μPIV using the equation $\omega = \nabla \times v$. The vorticity distribution is shown as a heat map overlay on the streamlines in Fig. 5. At $Re = 3$, we observe small microvortices at the entrance to the channel. At $Re = 6$, the strength of the vortices increases twofold and the location of flow separation moves further downstream. At higher Re ($=12$ and 18), the strength of the vortices increases further by several folds, and the point of flow separation is pushed further downstream from the entrance. However, the extremely high flow velocities closer to the center of the channel precluded particle tracing at these locations.

The presence of fluid vortices without any RBC at $Re = 3$ and 6 suggests that other blood components may be transported into

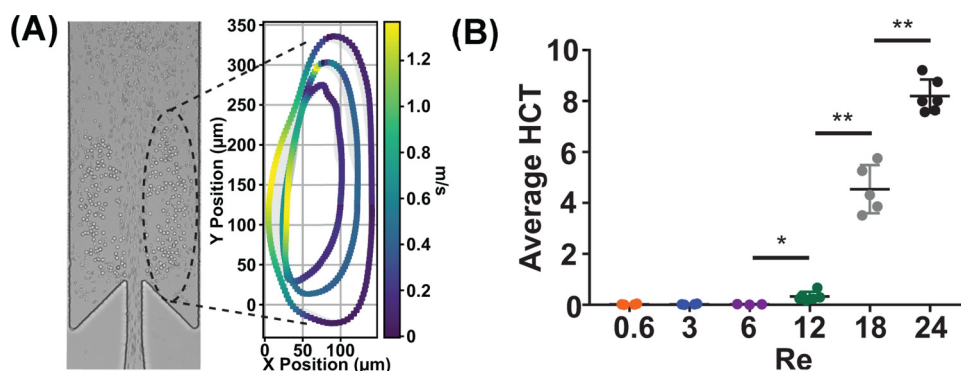


FIG. 4. RBCs in vortical flows. (a) Trajectories and velocities of RBCs within the vortices at $Re = 18$. The centroid of RBCs in the vortices was tracked frame by frame at 10 068 fps, and their velocities were computed. The RBCs were seen to be in continuous motion upon entering the vortices and followed a limit cycle. The data are based on the average of five RBCs for each limit cycle; (b) average of local HCT within the vortex during steady circulation in vortical flows, obtained by summing over local hematocrits in the vortices, represented as mean \pm SD ($n = 3\text{--}6$, $*P < 0.05$; $**P < 0.01$).

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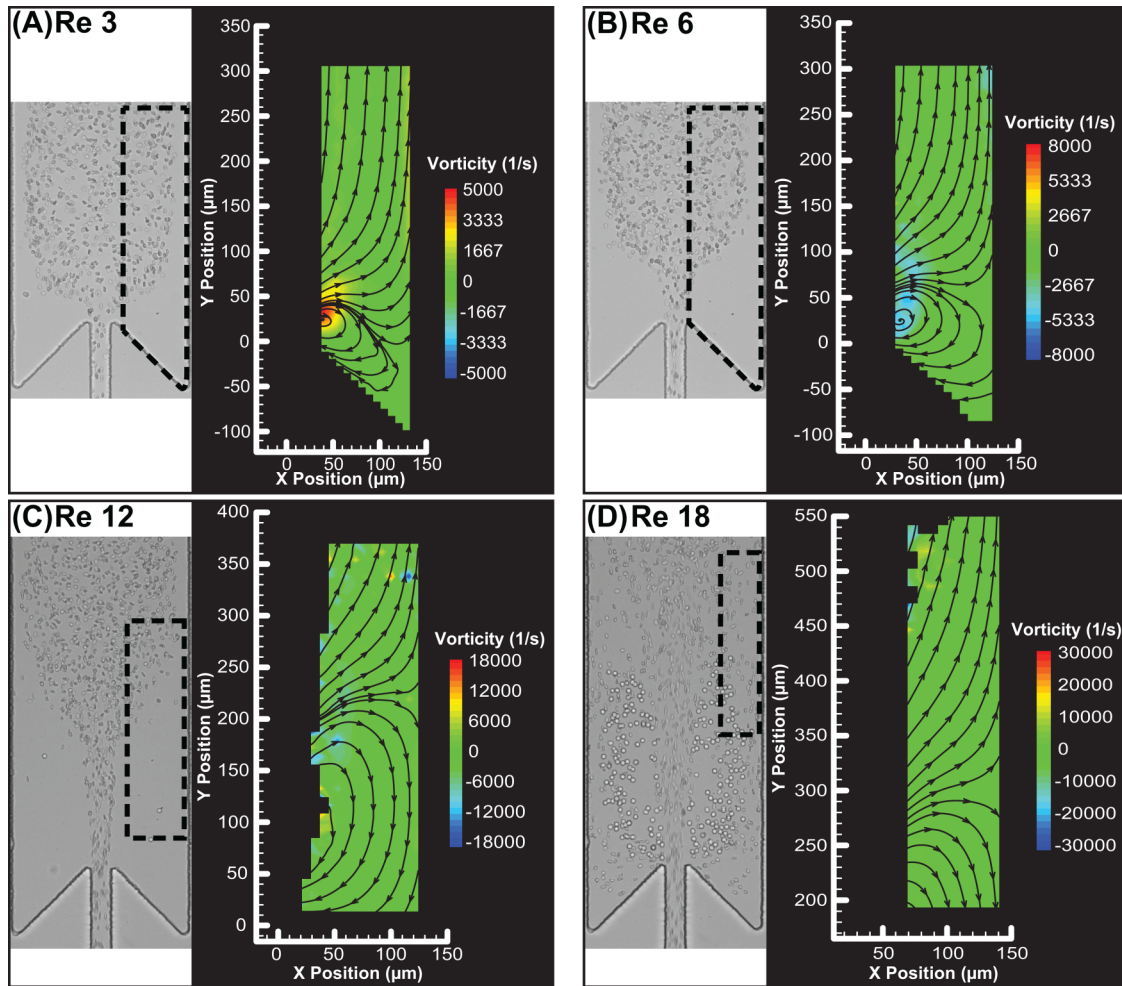


FIG. 5. Streamlines and vorticity distribution in vortical flows. From the μ PIV measurements of instantaneous velocities, streamlines and vorticities were computed at the indicated locations at the various Re numbers (a)–(d). RBC distributions from high speed imaging are also shown. The images show that although there is a significant vorticity as seen at Re = 3 and 6, the recirculation of RBCs does not begin until the Reynolds number reaches 12. The point of flow separation advances downstream with an increase in Re. At Re = 12 and 18, particle tracking was possible only at locations where the flows were not too high.

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the venous valve sinuses. Unlike other studies where RBCs were used to follow fluid streamlines, in this work, the fluid vortices were tracked with smaller particles of size similar to that of platelets ($1\ \mu\text{m}$) and stiffer than the RBCs. Our observation at Re = 3 and 6 implies that while RBCs may not enter the valve pockets at these low flow rates, smaller platelets may preferentially enter the valve regions. Computational and experimental studies have shown the margination of platelets driven by cell–cell collision or volume exclusion, wherein more deformable RBCs drive less deformable platelets toward the wall.^{24,30,31} Our results show that platelet margination can be a flow-driven phenomenon by transport along the streamlines and can happen independent of volume exclusion or due to collisions with RBCs.^{22,32,33}

Flow separation results in atypical wall shear stress

The presence of forward and reversing velocity profiles due to flow separation shown in Fig. 5 suggests that there are regional variations in shear stress on channel walls. The shear rate distribution is computed from the velocity vectors, using the equation $\varepsilon_{xy} = 1/2(\partial v/\partial x + \partial u/\partial y)$, where u and v are instantaneous local velocities in the x and y directions, respectively. Based on the μ PIV measurements, we estimated the shear stresses along the outer walls at the various Re numbers (Fig. 6). At a low Re, Re = 0.6 (orange line), the wall shear rates are low due to unidirectional creeping flows. At Re = 3 and 6, the flow separation and vortices result in a stagnation point [as shown in Figs. 5(a) and 5(b)],

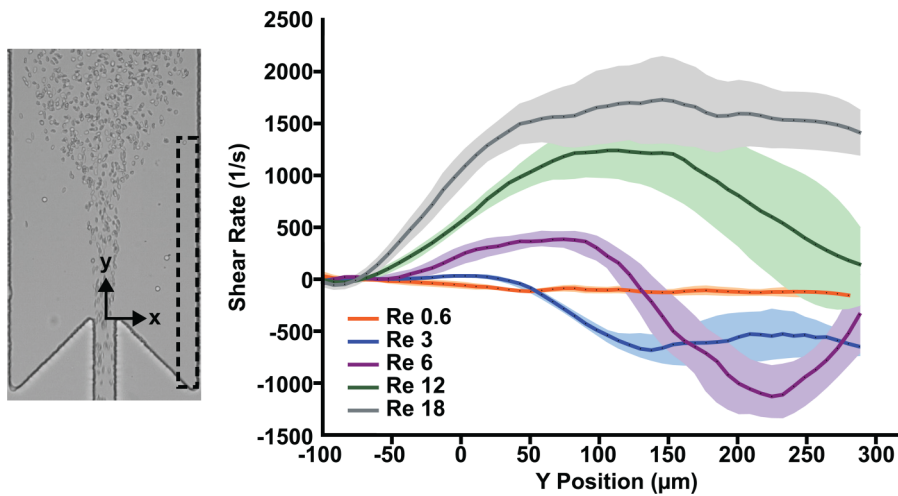


FIG. 6. Wall shear rate distribution. The shear rate distributions near the wall in the recirculation regions were obtained from the μ PIV measurements of instantaneous velocities at the indicated Re. For the chosen coordinate system, on the right wall, the shear rates are negative for forward flows and positive for reverse flows; and zero shear indicates stagnation point. The data are mean and SEM ($n = 3$).

and the wall experiences both flow reversal and forward flow. Correspondingly, the wall shear stress shows a non-monotonic profile with zero shear stress stagnation point at a location less than one channel width ($\sim 200 \mu\text{m}$). As the Re was increased further to $\text{Re} = 12$ and 18 (green and gray), the large backflow near the wall resulted in a high reverse shear stress at the wall, with the stagnation point moving further downstream. These data suggest that even at Re as low as 3, the walls may experience reversal of shear stress. Such regional variations in wall shear stresses may have important consequences on endothelial mechanotransduction and hence on its phenotype. Low flows in the venous valve region drive endothelial cells to a low grade inflammatory and prothrombotic phenotype. This phenotype supports the adhesion of monocytes, which, in turn, is a rich source of tissue factor and initiation of intrinsic pathway of coagulation.³⁴ The hypoxia induced by low flows may also play a role in initiating thrombus development due to its effects on endothelial cells.³⁵

Estimation of threshold shear rates that drive RBC distribution in valve pockets using μ PIV and 3D CFD simulations

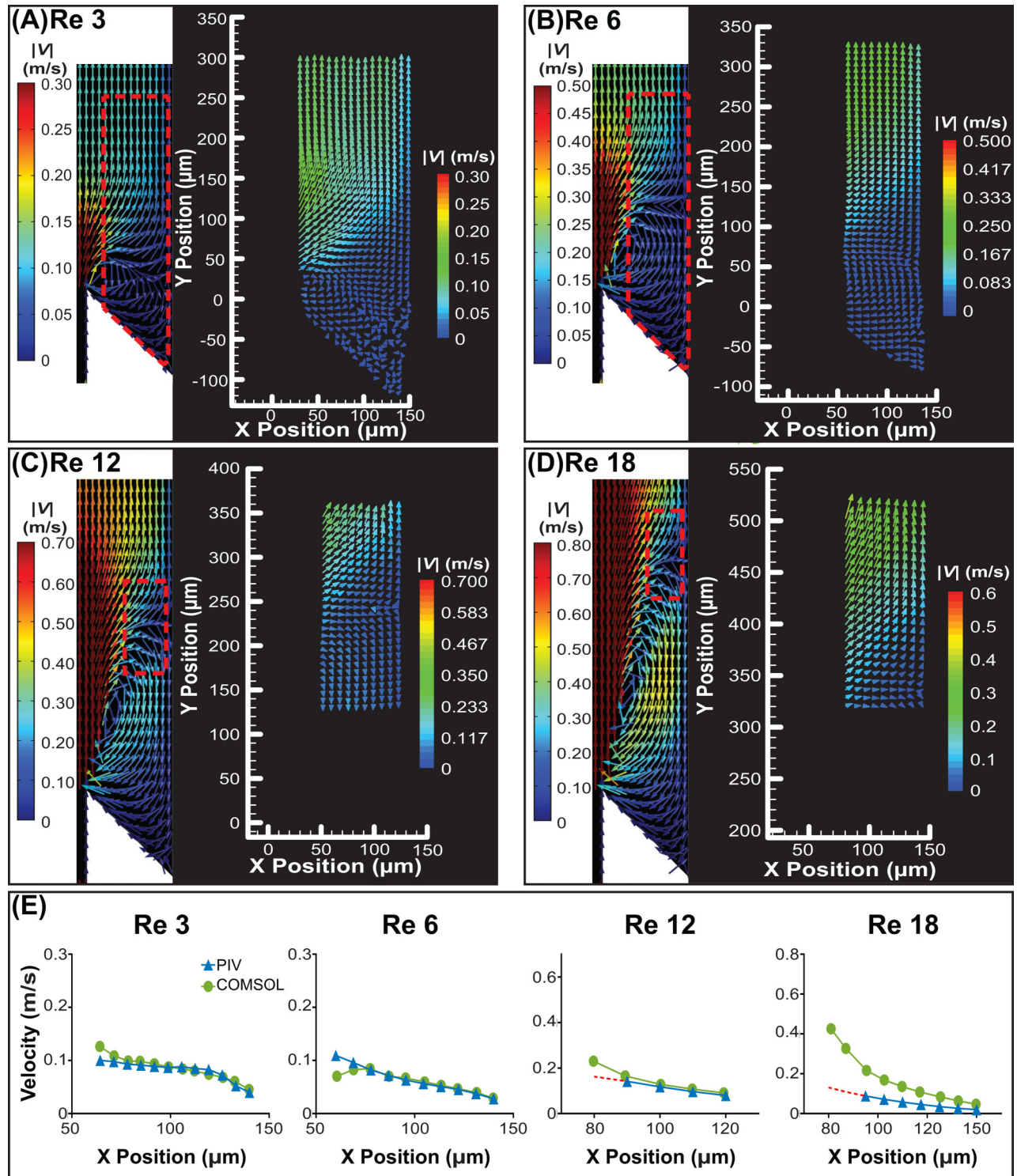
Since no RBCs were seen in the vortices till $\text{Re} = 12$, the cell trajectories do not follow the fluid streamlines in the vortex. When $\text{Re} < 12$, the cells do not cross streamlines to enter the vortices, suggesting that only at $\text{Re} = 12$, the energy necessary to drive the RBCs from the main flow to the vortex is realized. In a bounded Poiseuille flow, particles migrate toward the wall and occupy an equilibrium position due to the balance between the shear-gradient-induced lift force, which pushes the particles toward the wall, drag force due to the motion, deformation-induced lift force, and the wall-effect-induced lift force due to the wall, which act in the opposite direction, pushing the cells away from the wall.³⁶ For straight channel flows with a rigid particle, the shear-gradient-induced lift force expression is given as $F_L = C\rho G^2 a^4$, where C , ρ , G , and a are the lift coefficient, fluid density, local shear rate, and particle radius,

respectively.³⁷ Although the numerical validity of this expression may not be accurate for suddenly expanding flow with deformable cells, the scaling laws have been found to be applicable and used for vortex-based fractionation of cells based on their sizes.^{36,38–40} Next, the deformation-induced lift force is dependent on RBC deformability, which is a function of shear rate through the Capillary number (Ca) of a RBC, which is defined by $Ca = \mu\dot{\gamma}a/\sigma$, where μ , $\dot{\gamma}$, a , and σ are the fluid viscosity, shear rate, RBC radius, and shear modulus of the RBC membrane, respectively.⁴¹ Finally, the cell-cell interactions also depend on shear rate.⁴² Therefore, for a given particle size, the net lift force on a RBC will be determined by the local shear rate.

To obtain further insights into this lift phenomenon on RBC motion in vortical flows, we sought to estimate the shear strain acting locally on the cells. Although at low Re ($\text{Re} = 0.6$ and 3), we were able to obtain the complete velocity profile from μ PIV in the flow separation regions, at higher Re ($\text{Re} = 12$ and 18), the high velocities near the center of the channel precluded the tracking of particles and hence local velocities, which could only be obtained farther from the center, and farther from the regions where flow actually separates. Therefore, we used 3D CFD simulations to obtain velocity profiles in regions that were not feasible to obtain experimentally. We used COMSOL to solve the Navier-Stokes equation to obtain three-dimensional (3D) velocity vectors and compared it with μ PIV measurements (Fig. 7). These computations faithfully confirm the velocity profiles estimated using μ PIV including creeping flows at $\text{Re} = 0.6$; development and growth of microvortices at $\text{Re} = 3$ and $\text{Re} = 6$, respectively; and the formation of vortices and stagnation points near the wall at higher Re ($\text{Re} = 12$ and 18) (compare with Fig. 5). In particular, we note that the velocity vectors from CFD simulations match well at the various locations where experimental data were available and the local velocities were within the sensitivity limits of μ PIV [Fig. 7(e)].

Having matched the experimental and computational velocity fields either fully, at low Re, or partially at higher Re, we computationally determined the shear strain acting on the RBCs near the

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FIG. 7. Comparison between velocity distributions obtained from μ PIV measurements (right) with 3D CFD simulations (left) at the indicated locations and at the indicated Re (a)–(d). The dotted line in the velocity profiles (E) indicates discrepancy between experiment and simulation.

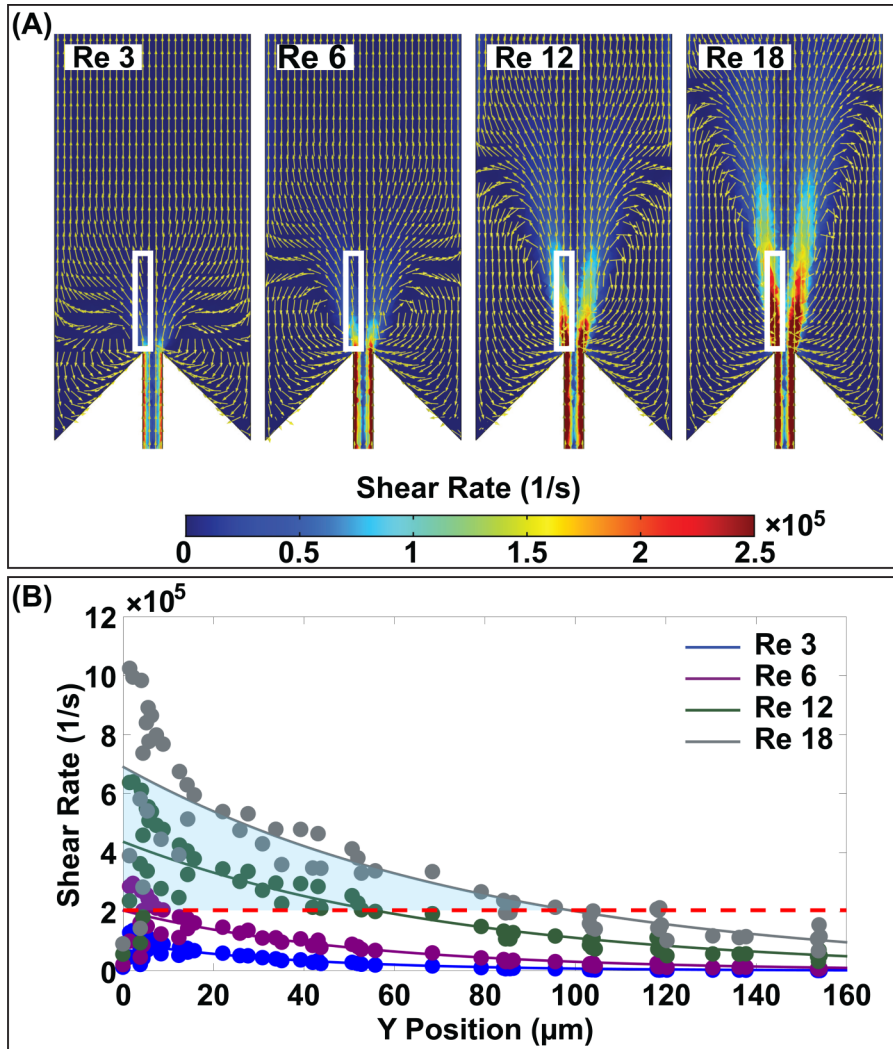


FIG. 8. (a) Shear rate distributions computed by 3D CFD simulations at the indicated Re. The white box indicates the location where the flow separation was noticed and, hence, was used in estimating location shear rates; (b) shear rates along at different Y-coordinates moving with the flow in the white box indicated in (a). The filled circles indicate the shear rates computed by the simulations at any given Y-coordinate, and the curves indicate the best fit. The red dotted line indicates the maximum shear rate corresponding to Re = 6, below which no RBC entered the vortical flows.

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entrance to the channel from where cells enter the valve pockets [Fig. 8(a)]. Figure 8(b) shows the shear rate perpendicular to the direction of main flow, plotted along the direction of flow at the y-location corresponding to the edge of the constriction at the inlet [within the white-bounded region in Fig. 8(a)]. We profiled the strain rates because the inertial boundary layer separates along this line to form laminar vortices (i.e., Moffatt corner eddy flow) in the sudden expansion. As expected, the strains continue to decrease as the fluid enters the sudden expansion, and at any given location, increases with an increase in Re.

Since we observed flow separation at Re = 3 and 6, but RBCs do not enter the vortices at these flow rates, we propose that a shear rate lower than the maximum value at Re = 6 ($\sim 1.8 \times 10^5 \text{ s}^{-1}$) is not sufficient to drive the RBC into the vortex [Fig. 8(b), dotted line]. But at Re = 12, when the shear rate increases to $2.5 \times 10^5 \text{ s}^{-1}$ or $\sim 200\text{--}250 \text{ Pa}$ (for a viscosity of 1 cP), a few RBCs enter into the vortices, suggesting that this value represents the necessary

sideward momentum to drive RBCs into the valve pockets. The increase in Re to 18 and 24 increases the shear rate linearly but the lift force by square of the shear rate, thus resulting in driving many RBCs into the vortices, resulting in a vortex hematocrit instead of a feed hematocrit.

The scale-down experimental system is appropriate to investigate the transport phenomena of RBCs isolated from small volumes of fresh human blood without relying on a substitute. Yet, it places certain limitations in translating the results to larger, actual venous valves. As mentioned previously, by matching the Re, we maintained flow patterns and regime in the scale-down model similar to those in femoral and saphenous veins. This means that the flow velocity and shear rates in the smaller microchannels are larger than those in *in vivo* veins. Hence, compared with the model, RBCs in venous valves will not only travel at lower velocity but will also experience different levels of lift forces. Another inherent constraint in the scale down model is the confinement-related

effects since RBC deformability is known to be altered in cell-sized channels.⁴³ Although we do not expect confinement effects at a single cell level in our microchannels since they are $\sim 6\times$ larger than the hydrodynamic diameter of RBCs, it is plausible that these effects may be felt due to cell–cell interactions. Therefore, the shear rate–vortical dynamics relationship in venous valves may be different from what is observed in our model microchannels due to the aforementioned scaling effects.^{44,45} Nonetheless, the experimental flow patterns and RBC distribution data presented in this work, together with our recent report on RBC deformability,⁵⁰ can be valuable for understanding RBC entrapment in venous valves, such as through computationally intensive multiscale simulations.⁴⁶

It is appropriate to note some of the experimental adaptations in this *in vitro* study that limit the applicability of our conclusions directly to the pathophysiology of venous thrombosis. We have used dilute red cell suspensions which are $\sim 10\times$ lower than physiological RBC concentrations so as to isolate fluid–cell interactions on RBC distribution. However, at higher RBC concentrations, cell–cell interactions may dominate fluid–cell interactions, and the local changes in hematocrit may be even more pronounced than what is reported in this study. We have used steady flow that does not capture pulsations, which are believed to be prominent due to muscle contraction, and can affect the dynamics of RBC entry and exit from the vortex.^{47,48} Furthermore, we have used stiff valves with an elastic modulus that is tenfold higher than healthy valve tissues; and we have used a valve expansion ratio of 1:10, while the expansion ratio for a healthy valve is 1:4. Of interest, the valve tissue becomes stiffer with aging due to fibrotic tissue formation, and the stiff valve does not open fully in response to pressure drop. Future work will extend to μ PIV measurements to investigate the impact of pliable valves and expansion ratios on RBC transport while accounting for RBC deformability, RBC distribution, confinement effects, and cell–cell interactions.

CONCLUSION

In summary, we have shown that vortical flows in microchannels of geometry similar to venous valve pockets result in anomalous local RBC distribution, which can be significantly different from the feed or bulk hematocrit. We have also shown that shear rates determine whether RBC trajectories follow fluid streamlines into the microchannel pockets. The μ PIV-based quantification shows small recirculating flow regions that do not contain RBCs and regions with RBCs that are trapped in infinite limit cycles.⁴⁹ Finally, the vortical flows also result in stasis and reversal of shear rate directions on the vessel walls. These findings illustrate that vortical flows due to sudden expansion can alter the local composition of cellular components and also local shear rates, thus influencing all three vertices of Virchow's triad implicated in mural or device-related thrombosis. Beyond relevance to venous thrombosis, our findings also provide experimental insights into inertial flow of dilute suspensions in sudden expansions, which has applications in microfluidics-based flow focusing for the separation of cells based on size or deformability. Our data provide shear rate thresholds for inertial focusing of cells into the expansions and increasing the separation efficiency by trapping them into the micro-vortices based on their size.

SUPPLEMENTARY MATERIAL

See the [supplementary material](#) for bright field images at Re 0.6–24, the calibration curve, and an experimental video showing RBC entrapment.

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AUTHOR DECLARATIONS

Conflict of Interest

The authors have no conflicts to disclose.

Ethics Approval

Venous blood was freshly drawn from healthy volunteers after signing an informed consent and obtaining written ethics approval in accordance with the approved Institutional Review Board (IRB) protocol (IRB F16134, Office of Research, SJSU).

Author Contributions

Z.A.C.S., V.V., L.R., and A.K.R. designed the research, analyzed data, and wrote the manuscript. Z.A.C.S., V.V., and D.M.V. performed experiments, analyzed data, and prepared the graphs. L.R. and A.K.R. contributed reagents and secured funding. Z.A.C.S. and V.V. contributed equally to this work. All authors approved the final version of the manuscript.

DATA AVAILABILITY

The data that support the findings of this study are available within the article and its [supplementary material](#).

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