# Production of Oligosaccharides from Pine Nut Shells by Autohydrolysis

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## Abstract

*Pinus pinea* nuts are commercial relevant Mediterranean edible forest nuts, with an increasing production and market value, whose industrial processing yields a lignocellulosic by-product, the pine nut shells, currently only used for combustion. Little research has been done on pine nut shells that could support a value-added application for this residue. This work studies for the first time the production of oligosaccharides by autohydrosis, and aims at an integrated upgrade within the biorefinery framework. Autohydrolysis was explored in the temperature range between 150 and 230 °C (corresponding to severity factors 2.13–4.63). Oligosaccharides, mainly xylo-oligosaccharides (95% of the total), were the key soluble products, reaching 28.7 g/100 g of xylan of the feedstock at the optimal conditions (log $R_0$ 4.01). Other products were monosaccharides and phenolic compounds that reached 7.8 and 4.7 g/L, respectively, under the most severe conditions. The stability of the oligosaccharides at different temperatures (room, 37 °C and 100 °C) and pH (between 1 and 11) grant them significant market potential in the food and pharma sectors. The pre-treated pine nut shells by autohydrolysis presented an improved, although low, enzymatic digestibility (14%), and an improved high-heating value, therefore advising their further valorization by thermochemical pathways.

**Keywords** Biorefinery · Hemicellulose upgrade · Oligosaccharide stability · Pre-treatment · Xylo-oligosaccharides

## Introduction

*Pinus pinea* L. (stone pine) is a softwood species, cultivated in a total area estimated at 600,000 ha, distributed in the Mediterranean region and particularly important in the Iberian Peninsula due to its adaptability to moist but well-drained soils in coastal sandy areas suffering little temperature variation [1]. Although *P. pinea* trees may be used for timber production, they are mostly valued for production of their edible seed kernels, the pine nuts, which have a significant economic importance and a high, and increasing, market value. Production of pine nuts represents the most valuable and profitable activity for the stone pine plantations in Spain, Portugal, Italy, and Turkey, increasing the economic development of the rural areas where they grow.

The commercial production of pine nuts starts with the field collection of the pinecones where the seeds are enclosed. In the processing mills, the pinecones are opened and the seeds extracted, followed by the crushing of the hard lignocellulosic shells that enclose the pine kernels or pinions, which are the high-valued commercial product. The pine nut shells represent about 77% of the seed mass and make up an agro-industrial by-product that is produced in large quantities and concentrated at the nut-processing mill, thereby enabling their easy management [2]. The use of side mass flows from production of edible nuts is increasingly receiving attention under the concept of full resource use and zero-waste chains, and many research works have studied, e.g., almond, walnut or peanut shells, among others. A recent report estimated a world availability of waste pine nut shells of 114 thousand tons per year [3].

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Comparatively to other nut shells, less studies have considered pine nut shells and evaluated their potential for production of added value products, and currently, they are used only as a low added-value energy source directly for combustion. Most existing works are related to the thermochemical conversion for the production of bio-oil [4], activated carbons [5], and biochar [6] while steam distillation was tested to produce essential oils with application in foodborne diseases [7]. There are only a few works related to the chemical characterization of this hard and brittle material, reported to have a high lignin content of 40.5%, a significant proportion of xylan in the hemicellulosic fraction (xylose amounts to 65% of the non-glucose monosaccharides), a moderate content of extractives (4.5%), and low ash [2], thereby chemically differing from other nut shells. A very recent study with *P. pinea* pine nut shells from Turkey also reported low ash (1.7%) and extractives (4.2%) and a high Klason lignin content (52.2%) [3]. As such, the chemical composition of the pine nut shells suggests a potential valorization based on the upgrade of its hemicelluloses and lignin fractions.

The biochemical platform of biorefineries is an advantageous pathway to produce high value-added products, namely focused on the valorization of hemicelluloses that requires a selective fractionation of the structural macromolecular components. Hydrothermal processes such as autohydrolysis have been one of the best choices for this purpose since no chemicals other than water are used, and limited equipment corrosion and low by-product generation are expected to occur. Autohydrolysis has been applied on several biomass materials, allowing a high recovery of solubilized hemicelluloses, specifically as oligosaccharides [8, 9]. Monomeric sugars, acetic acid, and phenolic compounds are also obtained together with a minor production of sugar degradation compounds (e.g., furfural, 5-hydroxymethylfurfural, formic, and levulinic acids) [10]. The solid lignocellulosic fraction remaining after autohydrolysis, containing cellulose and lignin, can undergo further valorization, namely through delignification processes and cellulose enzymatic hydrolysis to produce glucose, and lignin-derived phenolic compounds, while also not excluding a direct use for energy, e.g., in co-generation [11, 12].

The composition and structure of the oligosaccharides obtained by autohydrolysis, namely regarding chain length, branching degree, monosaccharide composition, and overall purity in the liquid stream, are influenced by raw material and process conditions, thereby allowing targeted production for a wide range of applications [13]. Many studies have focused on xylo-oligosaccharides (XOS) since they have biological activities such as antiallergy, anti-microbial, anti-infection, and anti-inflammatory properties, selective cytotoxic activity, immunomodulatory action, cosmetic, and a variety of other properties [14]. The food and feed industries are also targeting novel carbohydrates as new prebiotic oligosaccharides that may act as nutrients for the probiotic *Bifidobacteria* and *Lactobacilli* [15, 16] and can be recognized as functional oligosaccharides [17]. Furthermore, they also are used as low-sweetness humectants [14, 17, 18]. Studies have also shown that XOS have the potential to reduce serum cholesterol and triglycerides levels which are important indicators of cardiovascular disorders [19].

Pine nut shells have not yet been researched as a potential feedstock along such a biorefinery approach. The aim of this work is to evaluate the selective production of hemicellulosic oligosaccharides from pine nut shells using hydrothermal treatments (autohydrolysis) under various process conditions using the severity factor (log $R_0$) as treatment intensity measure. The results were analyzed in terms of yields obtained in the autohydrolysis liquors for oligosaccharides, monosaccharides, and by-products, and for cellulose and lignin recovery in the autohydrolysis remaining solids. Studies of oligosaccharides stability in the liquor and digestibility of the remaining solids was also conducted. The results presented in this work will be the first to be published for pine nut shells from *Pinus pinea* and aim at contributing to their valorization as a resource within a chemical platform of biorefineries.

## Material and Methods

### Feedstock

Pine nut shells from *Pinus pinea* L. were supplied by one industrial company in Portugal, as obtained from the nut processing. The pine nut shells were coarsely ground with a knife mill (Waring, Snijders Scientific, Holland), and screened for particle size characterization. The fractions retained between 1.00- and 3.55-mm wire openings were collected, homogenized in a single lot, and stored in a capped PE-plastic container, at room temperature.

### Autohydrolysis

The pine nut shells were mixed with water at a liquid-to-solid ratio of 3 (w/w, dry basis), to a total mass of 1.2 kg. A 2-L stainless steel reactor (Parr Instruments Co., Illinois, USA) with PID temperature controller (4842, Parr Instruments Co., Illinois, USA) was used for the autohydrolysis. The reaction was carried out under continuous agitation (150 rpm) and in non-isothermal operation up to 230 °C with a typical heating rate of 3.8 °C/min. Reaction was stopped when the desired final temperature was attained for the values between 150 to 230 °C.

After reaction completion, a rapid cooling was made (typically less than two minutes to reach temperatures below 100 °C), and the liquid and solid streams were separated by filtration (Whatman Nr. 41 filter paper), under vacuum. The solid residues were washed with 500 mL of distilled water and filtered once again. The effect of the treatment conditions is interpreted based on the severity factor, $\log R_0$, taking into account the full temperature profile, as detailed elsewhere [20] with $R0 = \int_0^t \exp\left(\frac{T(t)-100}{14.75}\right)dt$ where the temperature T (°C) is a function of time $t$ (min), and 14.75 is an empirical parameter related with activation energy and temperature. The following $\log R_0$ conditions were tested: 2.13, 2.80, 3.42, 4.01, and 4.63, corresponding to a maximum temperature of 150, 170, 190, 210, and 230 °C respectively.

## Chemical Analytical Procedures

The chemical composition of the pine nut shells feedstock and of the solids remaining after autohydrolysis were determined using standard procedures provided by the National Renewable Energy Laboratory (NREL) [21].

The composition of the autohydrolysis' liquid stream was carried out by HPLC with an Aminex HPX-87H column to quantify free monosaccharides, formic, acetic and levulinic acids, and furan derivatives (furfural and 5-hydroxymethylfurfural). Since galactose and mannose are co-eluted at the same time of xylose, therefore not allowing individual peak separation, it was assumed that the peak is mostly xylose [2].

Monosaccharides and aliphatic acids were quantified using a refractive index detector (RID), while furans were quantified using a diode array detector (DAD) using data obtained at 280 nm. Oligosaccharides were quantified indirectly after their hydrolysis to monomers using an aliquot of liquor subjected to quantitative acid hydrolysis. The methodology followed previously detailed protocols [21, 22].

The total phenolic compounds content of the hydrolysates was assayed spectrophotometrically at 765 nm by the Folin–Ciocalteu method [23] using a microplate spectrophotometer (Multiskan™ GO, Thermo Scientific, MA, USA) and gallic acid as calibration standard. The phenolic compounds were identified by capillary zone electrophoresis (CZE), as previously described [24].

## Stability of Oligosaccharides in the Liquid Fraction

Shelf life of the liquid fraction and of the solubilized oligosaccharides was measured in the hydrolysate obtained in optimal conditions. A defined volume was filtered through 0.45-µm Millipore® filters and kept in a dry place at room temperature away from light. At specific intervals (once a week), a sample was taken for chemical analysis to quantify the oligosaccharides content and optical microscopy inspection for the presence of microbial contaminants.

The oligosaccharides' stability to pH and temperature was also evaluated by applying a method previously developed in our laboratory [25], based on methods described in the literature [26]. First, the liquors were filtered (Millipore® filters with pore diameter 0.45 µm), divided into 500-mL wide-mouthed flasks and freeze-dried using a Labconco (USA) freeze-dryer, at – 35 °C. These purified OS were used for all the tests.

The oligosaccharides samples were dissolved in "buffer" solutions (Table 1), resulting in a concentration of approximately 100 g/L, and pH 1, and 3. The prepared solutions were placed in a thermostatic oil bath at 100 °C, during 1 h, and subsequently analyzed by HPLC to determine the stability of the oligosaccharides.

## Enzymatic Digestibility

The enzymatic digestibility of the feedstock and processed solids was carried out based on the NREL/TP-510–42,629 protocol [27]. This procedure consists in using a sample of biomass of 0.15 g that is digested in the presence of 5 mL of sodium citrate 0.1 M pH 4.8 buffer solution, 100 µL of a solution of sodium azide (2% w/v), as anti-microbial agent and Celluclast® 1.5 L, and Novozyme 188 enzymes in prescribed quantities to attain 60 FPU/g and 64 pNPGU/g of dry biomass, respectively. The volume was adjusted with distilled water to 10 mL considering that the biomass has a density of 1. Two blank assays were also prepared, to consider both the (i) sugars that may arise from the enzyme solution (blank assay carried out without added biomass), and (ii) the sugars derived from non-enzymatical biomass hydrolysis (blank assay carried out without adding enzymes) to correct the results for the free saccharides present in the biomass and products that could possibly be formed in the absence of enzymes.

The samples were placed in a 50-mL plastic, round-bottom, capped centrifuge tubes, and incubated at 50 °C, under orbital shaking (150 rpm) in an incubator (Comecta, Spain). After 72 h, the tubes were placed in a boiling water bath, for 5 min, to inactivate the enzymes. Finally, the samples were filtrated using nylon membranes (0.22 µm) and analyzed by

**Table 1** Preparation of the "buffer" solutions for the evaluation of the stability of oligosaccharides

| pH | Solution A | Solution B | Vol. Sol. A (mL) | Vol. Sol. B (mL) | Total Vol. (mL) |
|----|-----------|-----------|-----------|-----------|-----------|
| 1* | 0.2 M KCl | 0.2 M HCl | 50.0 | 97.0 | 200.0 |
| 3 | 0.1 M $C_6H_8O_7$ | 0.2 M $Na_2HPO_4$ | 39.8 | 10.2 | 100.0 |

*This solution is not a true buffer, but for simplicity thus considered in this work, similar to what is described in the literature

HPLC for the released sugars. All assays were performed, at least, in duplicate. The enzymatic digestibility was quantified by the ratio of digested cellulose to the initial cellulose content.

## Results and Discussion

The pine nut shells had the following chemical composition as determined using standard chemical summative analysis: 4.75% proteins, 3.04% ash, 2.67% extractives, 42.63% Klason lignin, 25.93% cellulose (as glucan), 20.98% hemicelluloses (as the sum of 16.27% xylan, galactan and mannan, 2.72% arabinan, and 1.99% acetyl groups).

The chemical composition of pine nut shells was previously determined by Queirós et al. (2019) and the reported values are similar to those obtained here, e.g., 4.5% extractives, 40.5% lignin, and 48.7% polysaccharides with the following composition: glucose 29.1%, xylose 12.7%, mannose 4.0%, galactose 1.2%, arabinose 1.2%, rhamnose 0.1%, 1.2% galacturonic acid 0.2%, and acetyl groups 0.3% [2]. Sen et al. (2022) also reported a similar chemical composition with 4.2% extractives and 52.2% Klason lignin [3].

### Effect of Autohydrolysis on the Composition of the Liquid Phase

Pine nut shells were subjected to the autohydrolysis process under non-isothermal conditions to final temperatures of 150, 170, 190, 210, and 230 °C, corresponding to severity factors of log $R_0$ 2.13, 2.80, 3.42, 4.01, and 4.63 respectively. Figure 1 shows the composition of the autohydrolysis liquor at the tested conditions as a function of the reaction severity (log $R_0$), regarding concentration of xylo-oligosaccharides and gluco-oligosaccarides (Fig. 1A), of the monosaccharides glucose, xylose, and arabinose, and acetic acid (Fig. 1B), and of furfural and 5-hydroxymethylfurfural (Fig. 1C).

Oligosaccharides were the main compounds in the liquor, especially for the intermediary severities, reaching a maximum of 16.5 g/L at log $R_0$ 4.01, which corresponds to 6.6% of the initial pine nut shell mass. The majority of the hemicellulosic oligosaccharides solubilized by autohydrolysis were xylo-oligosaccharides containing mainly xylose, and smaller proportions of arabinose, galactose, mannose, and of acetyl groups, reflecting the initial composition of the pine nut shells hemicelluloses. Gluco-oligosaccharides accounted for less than 5% of the total. Xylo-oligosaccharides concentration increased markedly from 0.98 g/L at log $R_0$ 2.0 to 14.88 g/L at log $R_0$ 4.01 (210 °C), corresponding to the increased xylan depolymerization into soluble oligomers with higher temperatures, but decreased abruptly after that to 1.10 g/L at $R_0$ 4.5, corresponding to the hydrolysis of the solubilized oligomers to monosaccharides. At the optimal
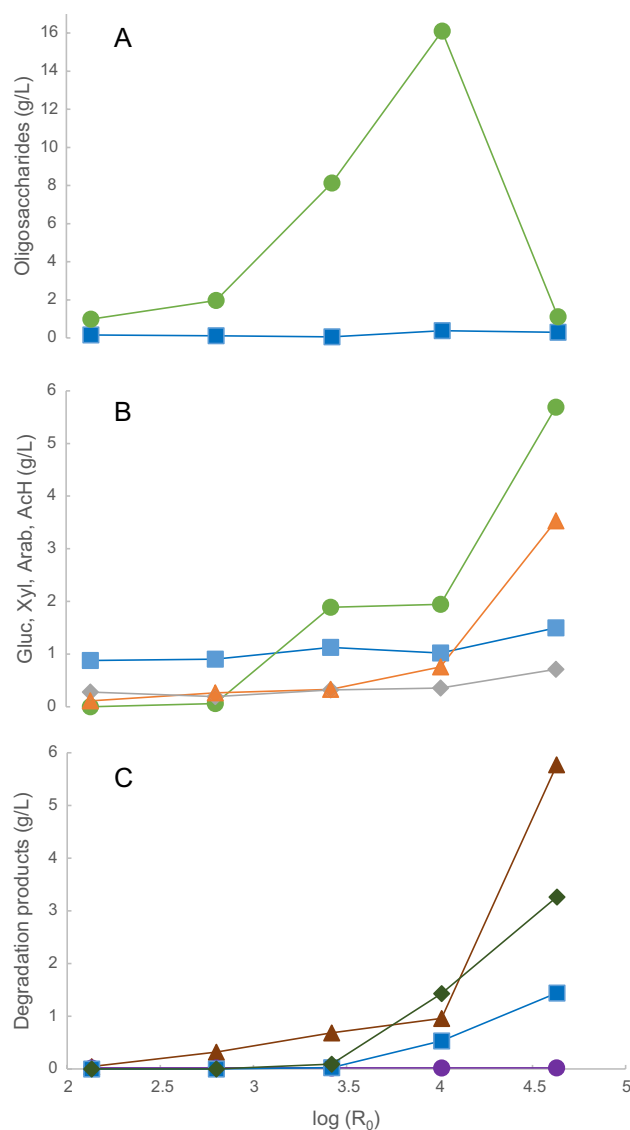


**Fig. 1** Concentration profile (g/L) of oligosaccharides, monosaccharides, acetic acid, and degradation products as a function of log $R_0$. plot **A**: ● hemicellulosic oligosaccharides, ■ gluco-oligosaccharides; plot **B**: Monomers ● xylose, ■ glucose, ◆ arabinose, ▲ acetic acid; plot **C**: ■ 5-hydroxymethylfurfural, ◆ furfural, ▲ formic acid, and ● levulinic acid. Lines are used for eye guidance only

conditions of log $R_0$ 4.01, the solubilization of xylo-oligosaccharides corresponds to a 28.74 g/100 g of xylan in the pine nut shell feedstock. This value compares with results obtained with eucalyptus wood but it is relatively low in relation to other biomasses like corn straw with values above 40% [8].

Nevertheless, the present results demonstrated that autohydrolysis of pine nut shells is a possible process to produce xylo-oligosaccharides, as it uses a low liquid-to-solid ratio of 3 with low loss of efficiency. This is a significant advantage in terms of cost reduction, as compared to the

common use of liquid-to-solid ratios of 7 to 10, as described in the literature [8, 10]. Low liquid-to-solid ratios (i.e., high solid loadings) offer many advantages since larger biomass amounts can be processed per unit operation, thereby allowing less capital costs in biorefinery implementation. Furthermore, the process will consume lower amounts of water and energy, making it more environmental and economic sustainable and also simplifying downstream processing [28].

The decrease of xylo-oligosaccharides concentration for the most severe condition tested is due to their depolymerization into monosaccharides and subsequent degradation products, as shown in Fig. 1. This has been observed in other autohydrolysis studies for severities above 4.0 and is consistent with previous results on wood, agricultural, and agro-industrial residues [8, 28–31].

The carbohydrate monomers resulting from depolymerization of hemicelluloses or of xylo-oligosaccharides increased gradually with severity, reaching a maximum of 6.40 g/L at log $R_O$ 4.67, mainly consisting of xylose (Fig. 1B). Similarly, xylose concentration increased from log $R_0$ 3.42 onwards, and acetic acid started to accumulate reaching 3.53 g/L, that corresponds to 94.8% of all the acetyl groups present in xylan.

Furfural and 5-hydroxymethylfurfural are degradation products of pentose and hexose sugars, respectively. Under the highest oligosaccharides-yielding conditions, both these furans had low concentrations, higher for furfural as compared to 5-hydroxymethylfurfural due to the higher amounts of pentose sugars in pine nut shell hemicelluloses, and the higher susceptibility of pentoses to undergo dehydration [26]. Other sugar degradation by-products such as levulinic and formic acid were also present, but in low concentrations, so that the total acid concentration (including acetic acid) for the optimal xylo-oligosaccharides production condition was below 2 g/L. Furans and acids are potential microbial inhibitors but their low concentration in the autohydrolysis liquors does not preclude their use for fermentation processes [32].

The hydrolysates were also characterized by the Folin–Ciocalteu method for quantification of the total phenolic compounds (Fig. 2), which mainly derive from lignin degradation [33].

The profile shows a significant increase in the content of phenolic compounds with increasing severities, reaching a maximum concentration of 4.7 g/L for the most severe condition tested at log $R_0$ 4.67. These results are consistent with previous studies on wood and other agricultural and agro-industrial residues, e.g., eucalyptus residues, wheat straw, and olive tree prunings that also yielded phenolic concentrations above 4 g/L for similar severities [34] and corn straw with a maximum phenolic concentration of 6.97 g/L at log $R_0$ 4.51 [8]. The total content of phenolic compounds under the optimal conditions for
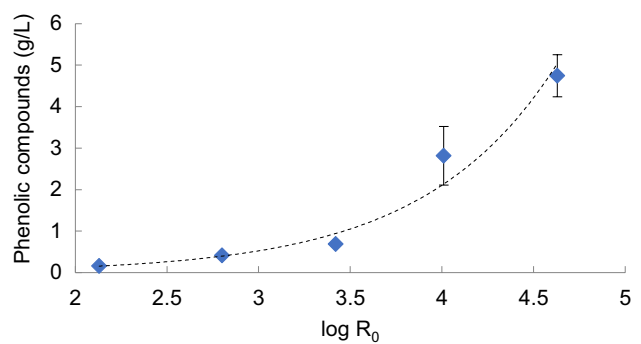


**Fig. 2** Concentration profile (g/L) of phenolic compounds in pine nut shells autohydrolysis liquors obtained with different severity conditions (log $R_0$). The bars show the standard deviation that was near zero for the first three points

xylo-oligosaccharides production does not preclude the use of the hydrolysis liquors in fermentation processes.

Several phenolic compounds with potential added-value applications, namely catechol, vanillin, vanillic acid, and 3-hydroxybenzoic acid, were identified in the hydrolysis liquors using CZE, especially for higher severity factors (log $R_0 \geq 3.42$). Although these compounds may be produced with higher yields by organosolv or alkaline delignification processes [11], the concentrations obtained in this work are significant, given the low liquid-to-solid ratio used. These compounds can be easily separated from the oligosaccharides by simple purification processes, such as membrane filtration [24].

## Hydrolysate's Shelf Life Evaluation

A possible industrial application of oligosaccharides must rely on their stability which is not trivial when they are stored in a liquid phase for a long time [35]. The storage stability of the liquor obtained under the optimal autohydrolysis condition at log $R_0$ 4.0 was studied at room temperature in a dark and dry place, without any type of microbial sterilization. Figure 3 shows the concentration of oligosaccharides present in the liquor depending on the storage time.

All oligosaccharides were stable during storage for at least 3 weeks, and no microbial contamination was detected. A similar evaluation of oligosaccharides stability was reported for *Annona cherimoya* hydrolysates with comparable results [25]. The absence of contamination in the liquors can be a consequence of the presence of furans, acids, and phenolic compounds, that can present a synergistic inhibitory effect of microbial growth [33, 36].

## Oligosaccharides' Stability

Oligosaccharides are mainly used in the food and feed sectors as prebiotic supplements, typically up to 10% (by
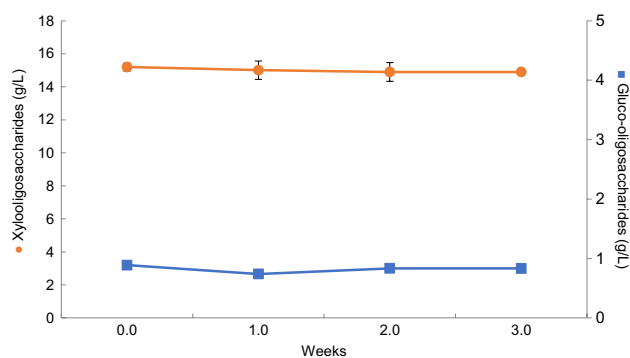
**Fig. 3** Stability profiles of the produced oligosaccharides (orang circle: xylo-oligosaccharides, blue square: gluco-oligosaccharides) measured as their concentration (g/L) for different storage times (weeks) at room temperature

weight) [35]. Their food use requires that they are as free as possible from metabolic inhibitors, such as furans (that are known carcinogenic and hepatoxic compounds) and aliphatic acids. Freeze-drying was tested as a liquor concentration and drying process for the oligosaccharides. This process also allowed removal of 89% and 85% of 5-hydroxymethylfurfural and furfural, respectively, and of 66% of acetic acid.

The stability of oligosaccharides was studied as a function of pH (1, 2, 7, and 11), and temperature (37 °C and 100 °C) by measuring the concentration in glucose and xylose before and after the stability tests. An increase of their concentration would mean a depolymerization of the oligosaccharides. The stability profiles of xylo-oligosaccharides and gluco-oligosaccharides at 100 °C for 1 h as a function of pH are shown on Fig. 4.

Both xylo-oligosaccharides and gluco-oligosaccharides were quite stable in the tested pH range. This is a particularly interesting result since oligosaccharides obtained from wheat bran or chicory were not so stable at pH 3 and 11,
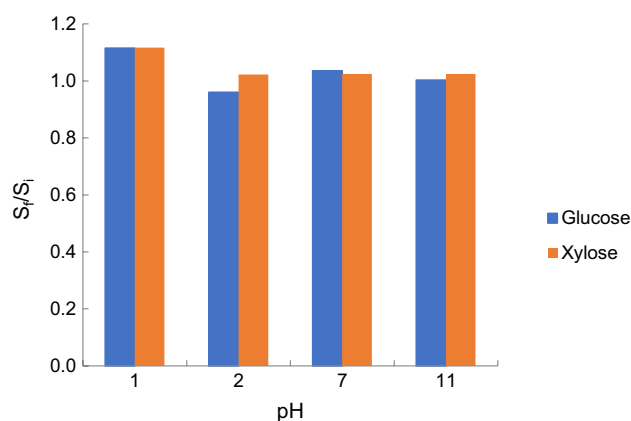
mainly those derived from chicory, which were sensitive to alkaline decomposition [35]. The oligosaccharides obtained from pine nut shells are therefore suitable for applications in the food industries and likely to be processed industrially.

The oligosaccharides ability to pass the human gut and reach the intestine should be evaluated when considering food applications, knowing that the stomachal digestive process occurs at 37 °C, for about 3 h, and pH values between 1 and 3. Under these conditions, the produced xylo-oligosaccharides showed no significant hydrolysis (data not shown). This was predictable according to the stability reported for other comparable compounds at 25, 37, and 50 °C under pH 1, 2, and 3 [37, 38], and this is also a first guarantee that their potential nutritional properties may be maintained when passing the digestive process.

Furthermore, these data also support that the purification of the obtained oligosaccharides may not require the freeze-drying step and potentially be achieved by evaporation or spray drying, which have significant techno-economic advantages.

## Effect of Autohydrolysis on the Composition of the Solids

Within a biorefinery framework, after the autohydrolysis treatment, it is necessary to find an application for the remaining biomass. Figure 5 shows the composition of the initial pine nut shells feedstock and of the processed solids after autohydrolysis with the different severity factors.

The mass loss, i.e., the solid solubilization induced by the autohydrolysis process was very low for the less severe conditions and the solids remaining showed a polysaccharide and lignin content very similar to that of the initial feedstock (Fig. 5). However, with the severity factor log $R_0$ 3.42, the solid yield decreased sharply to 79.8%. This decrease results from
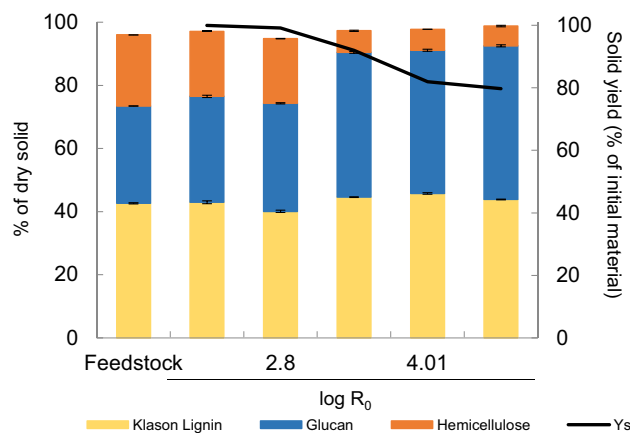


**Fig. 4** Stability at 100 °C of xylo-oligosaccharides and gluco-oligosaccharides measured as the ratio of the final monosaccharides ($S_f$) and the initial monosaccharides ($S_i$) as a function of pH



**Fig. 5** Pre-treated biomass yield (solid yield, Ys, in % of the initial pine nut shell) and chemical composition (% of the autohydrolyzed solid and of the initial pine nut shell) after autohydrolysis assays of pine nut shells as a function of the severity factor (log $R_0$)

solubilization of hemicelluloses which increased for the higher temperature tested, although the hemicelluloses were not completely removed due to the presence of slow-reacting xylan [39]. Conversely, arabinan was totally removed from the solid phase as well as acetyl groups that appeared in high concentration as free acetic acid in the hydrolysate for log $R_0$ 4.63 (Fig. 1).

The relative amounts of lignin and glucan in the solid residues increased with the autohydrolysis severity, i.e., the autohydrolyzed solids were enriched in lignin and cellulose. This is consistent with previous results showing a low effect of autohydrolysis on the solubilization of cellulose and lignin that therefore remain in the solid [8, 40].

A potential valorization route for the autohydrolyzed solids is their use for glucose production by cellulose hydrolysis, namely by enzymatic hydrolysis. Therefore, the enzymatic digestibility of the remaining cellulose in the autohydrolyzed solids is important for this evaluation. For this, enzymatic tests were performed using the enzymes Celluclast 1.5 L and Novozyme 188, and the results obtained for the autohydrolyzed solids with the different severity factors are shown in Fig. 6. The enzymatic digestibility increased slightly with autohydrolysis severity but reached only 14% of saccharification yield for the most severe treatment (log $R_0$ 4.63), and low glucose concentrations were obtained (1.07 g/L). The digestibility is lower than that reported for other materials with similar pre-treatment and enzymatic hydrolysis conditions, e.g., with the same enzymes, banana pseudostem pulp showed 90% digestibility [41], *Annona cherimoya* seeds 83% digestibility [25], and olive tree prunings and eucalyptus residues respectively 64.8% and 49.8% digestibility [34]. This high recalcitrance of pine nut shell cellulose to enzymatic hydrolysis may be partly explained by the high lignin content of the processed pine nut shells, as it is significantly higher as compared to the other reported materials as well as by the fact that it is a G-lignin [2]. Similar results were very recently published showing that extensive ball milling was required for lignin isolation by
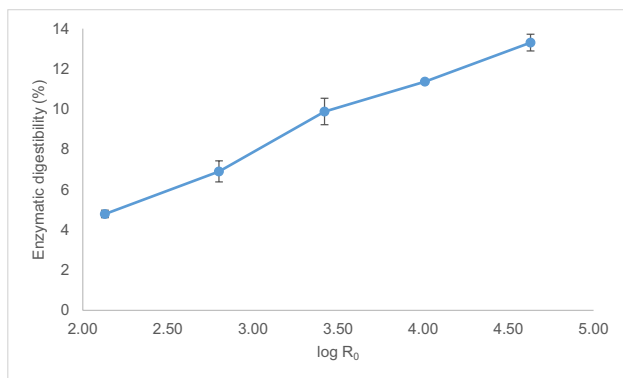
cellulose enzymatic hydrolysis from pine nut shells due to their recalcitrance [42]. The substrate capacity to adsorb the enzymes is also important and the compact structure of pine nut shells may not allow a suitable enzyme accessibility [43]. These results suggest that a delignification step after autohydrolysis and prior to the enzymatic digestion might be beneficial as it has been described for other materials [44].

Alternatively, the remaining cellulose and lignin-rich solid can be advantageously upgraded in the thermochemical platform of the biorefinery, targeting energy products [3–6]. Finally, combustion remains a possible utilization pathway, with the advantage given by an increased biomass high-heating value (HHV), favored by the high lignin and low hemicellulose content, and estimated at 19.0 kJ/kg [45].

## Conclusions

Pine nut shells can be processed by autohydrolysis at a low liquid-to-solid ratio to produce oligosaccharides, mainly xylo-oligosaccharides, in the liquid fraction under mild conditions (log $R_0$ 4.0) while higher severity autohydrolysis conditions (log $R_0$ > 4.6) extensively solubilized the hemicelluloses into monomers and promoted sugar degradation. The produced oligosaccharides kept in the hydrolysate were stable at room temperature for a 3-week period, without previous sterilization, and were chemically stable at 100 °C for 1 h and at 37 °C for 3 h, assuring the firsts traits for a potential use in the prebiotic market.

The autohydrolyzed pine nut shells were cellulose-lignin matrices showing recalcitrance towards cellulose digestibility, therefore directing their further valorization towards thermochemical pathways.

**Fig. 6** Enzymatic digestibility of the solid residue obtained from the autohydrolysis of pine nut shells with different severity factor (log $R_0$)

## Declarations

**Competing Interests** The authors declare no competing interests.

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