

## Introduction

### Motivation

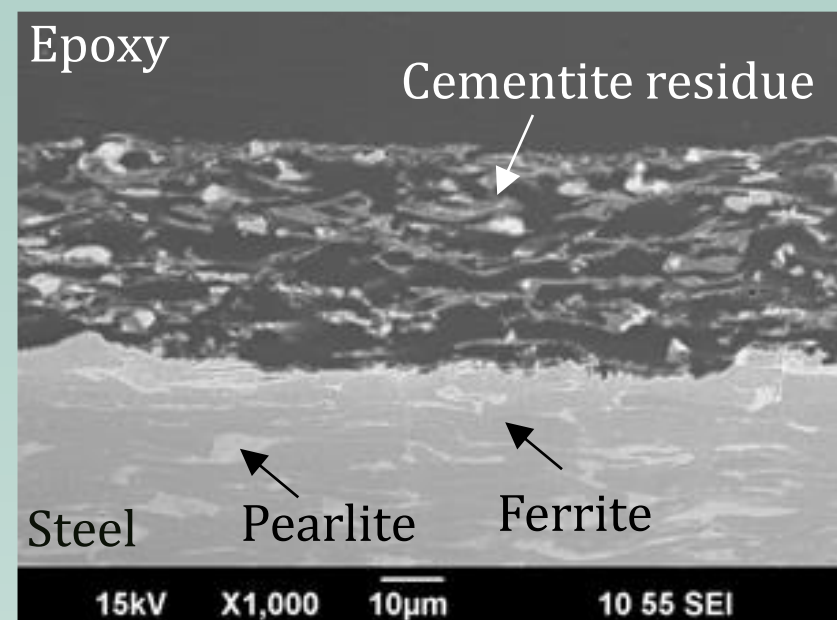
- Corrosion inhibitors (CIs) are widely used in the oil and gas industry to protect carbon steel tubulars against internal corrosion.<sup>1-3</sup>
- Various corrosion residues/products on internal wall of aged pipelines can affect the performance of corrosion inhibitors.<sup>4-6</sup>
- Residual cementite (Fe<sub>3</sub>C) has a detrimental effect on inhibition efficiency (IE) *via* serving as an additional cathodic area<sup>4-6</sup>, but the associated inhibition mechanism remains unclear.
- This effect varies with different types of corrosion inhibitor and steel<sup>6</sup> and has not been quantitatively evaluated.

### Objectives

- Quantitatively evaluate the effect of cementite on corrosion inhibition.
- Understand how the inhibition mechanism is influenced by cementite.

### Background

- During corrosion of carbon steel, ferrite dissolves and cementite remains on the surface.
- Cementite can accelerate corrosion rate (CR) *via* galvanic corrosion with ferrite owing to its electrical characteristics.



SEM images of cementite residue after pre-corrosion on C1018 steel with ferritic-pearlitic microstructure<sup>5</sup>

## Experimental

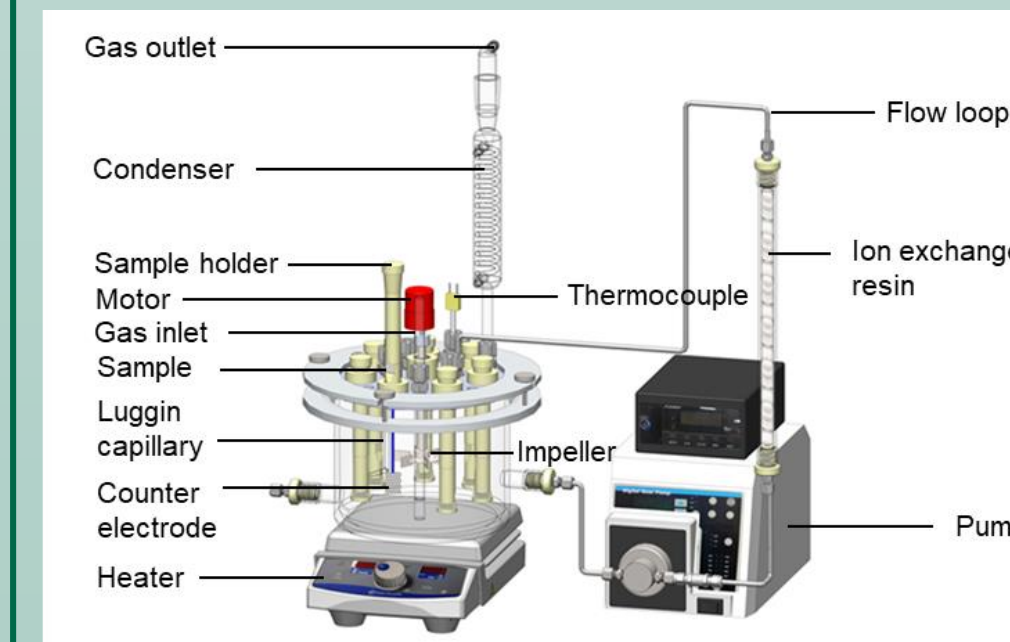
### Material and Chemicals

**Steel:** UNS G10180 carbon steel (C1018) with a ferritic-pearlitic microstructure.

**Corrosion Inhibitor:** Imidazolinium-type commercial package

### Experimental Equipment

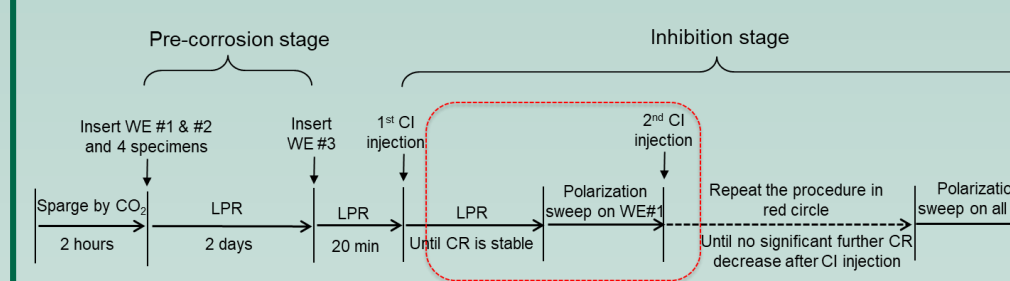
A glass cell with an impeller connected to a Fe<sup>2+</sup> concentration controller *via* a flow loop and up to 7 specimens being exposed in the test environment (immersion specimens and working electrodes).



### Test Matrix

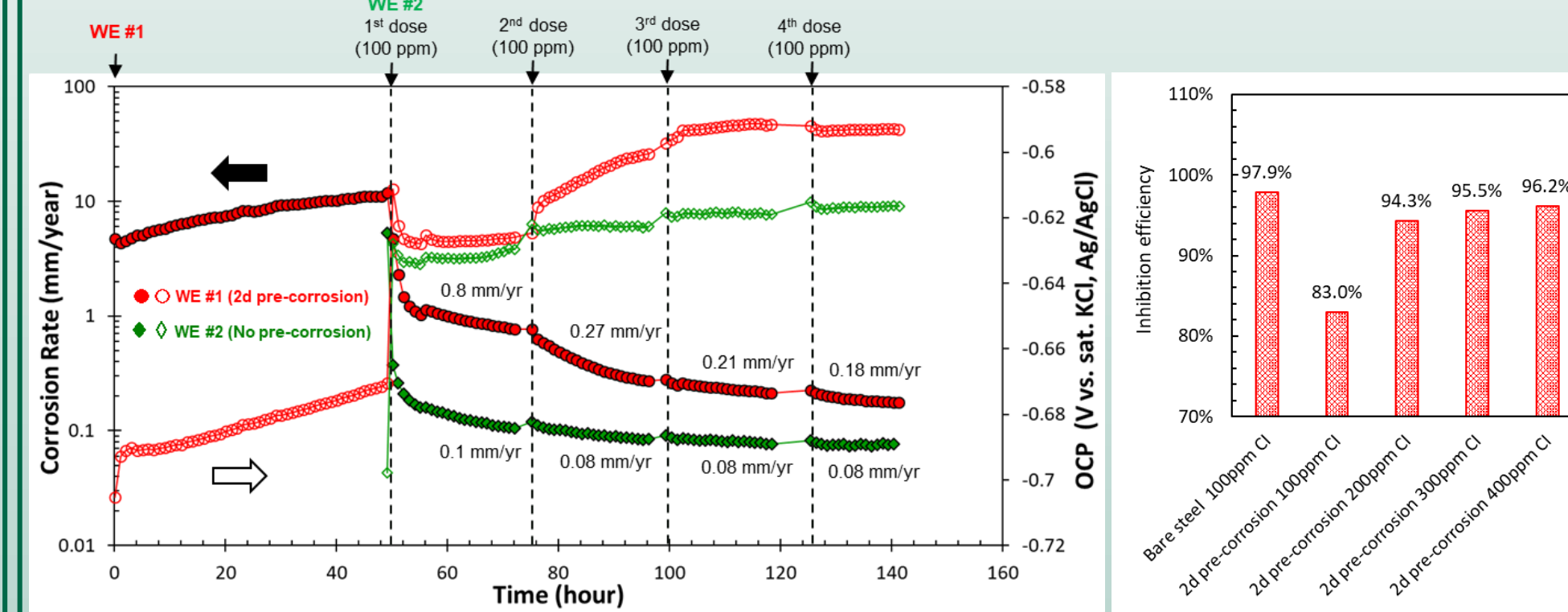
Parameters	Values
Electrolyte	5 wt.% NaCl
Working electrode	Flat square
Immersion specimen	Flat square
Temperature	55 ± 2 °C
Total pressure	1 bar
CO <sub>2</sub> pressure	0.86 bar (saturated)
pH	4.5 ± 0.1
Flow condition	Same mass transfer coefficient as flow of 1.61 m/s in a pipe with an ID of 0.1m (shear stress: 4.7 Pa)

### Procedure



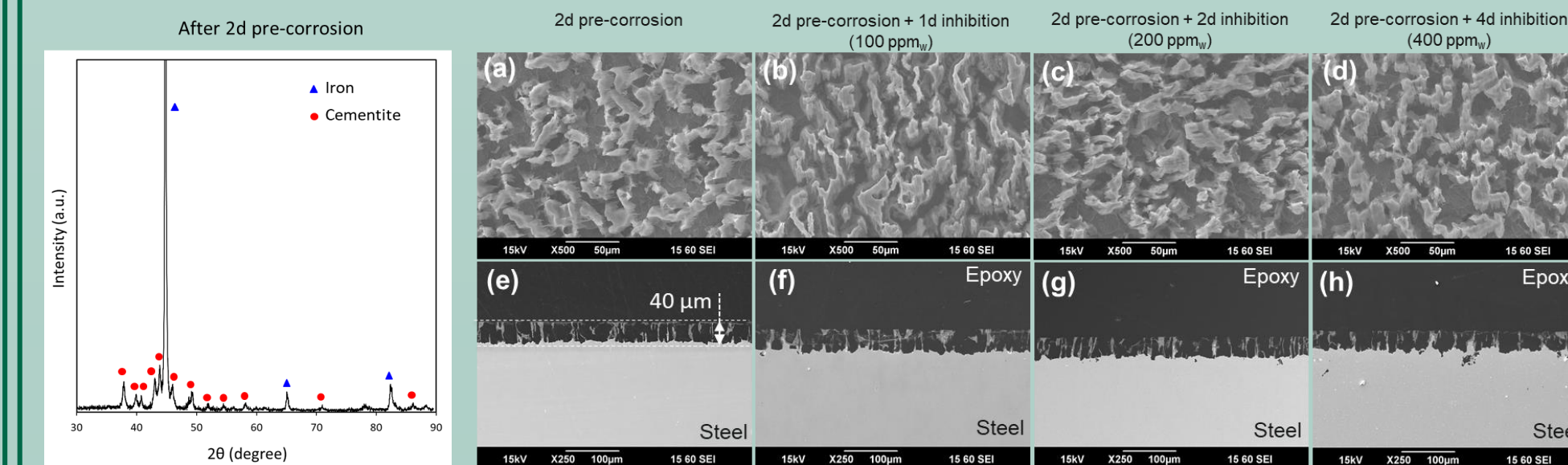
## Results

### Corrosion Rate & Inhibition Efficiency



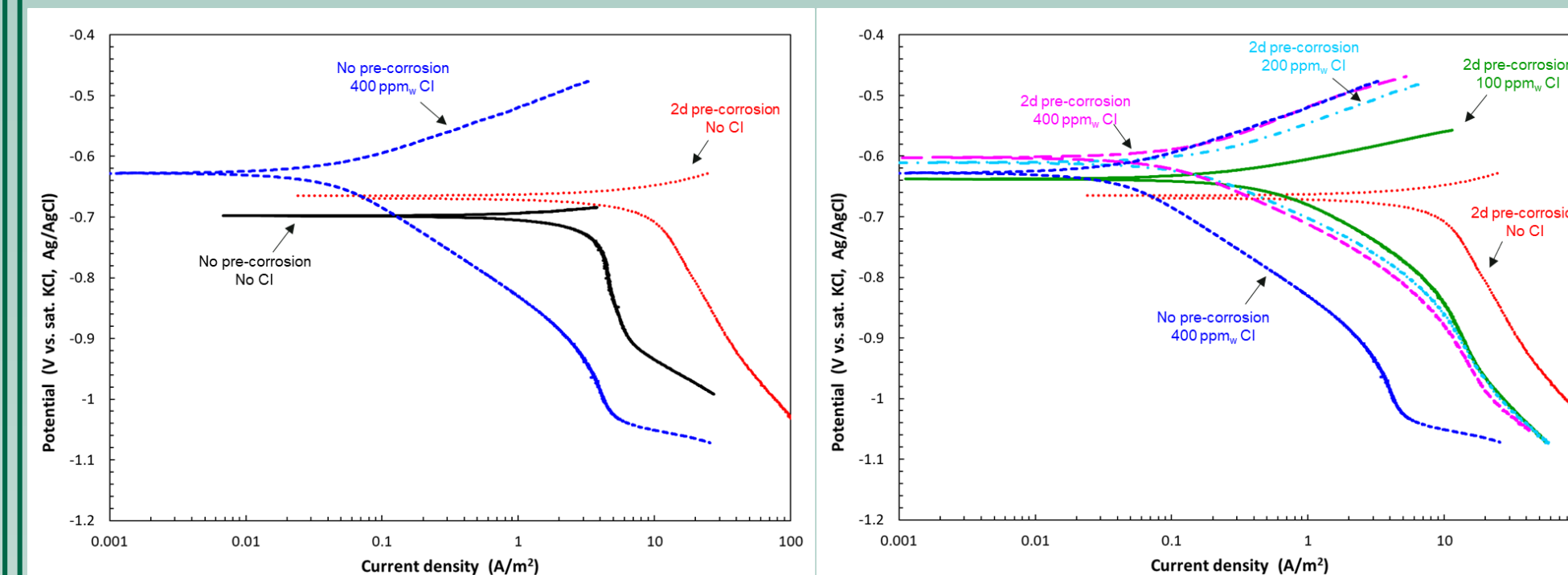
- IE was harmed after pre-corrosion and higher CI concentration helped to combat this detrimental effect.
- Minimum inhibited CR with pre-corrosion was higher than without pre-corrosion.

### Surface Characterization



A cementite skeleton remained on the specimen surface after pre-corrosion and its thickness remained the same indicating the effectiveness of the inhibition.

### Potentiodynamic Polarization



- After pre-corrosion, the cathodic limiting current was significantly accelerated.
- CI retarded both anodic & cathodic reactions and limiting current was unaffected.
- 400 ppm<sub>w</sub> CI retarded anodic reaction to the same extent as on bare surface, while cathodic curve showed a pronounced difference due to the cementite skeleton.

## Quantitative Evaluation

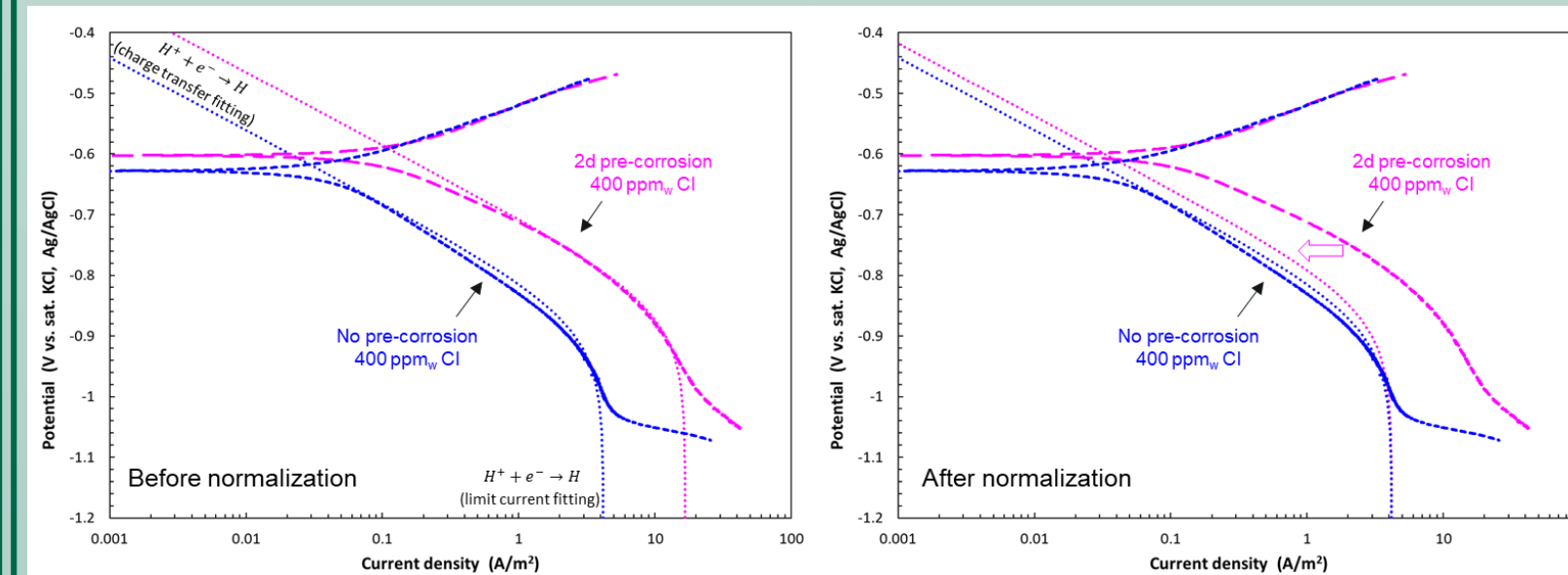
### Cathodic Polarization Curve Normalization

**Purpose:** Compare cathodic curves with and without residual cementite based on same cathodic reaction area.

**Method:** Cathodic curve with cementite will be normalized based on the cathodic area for the bare surface.

**Assumption:** The ratio of cathodic area with and without cementite was equal to the ratio of corresponding cathodic limiting currents.

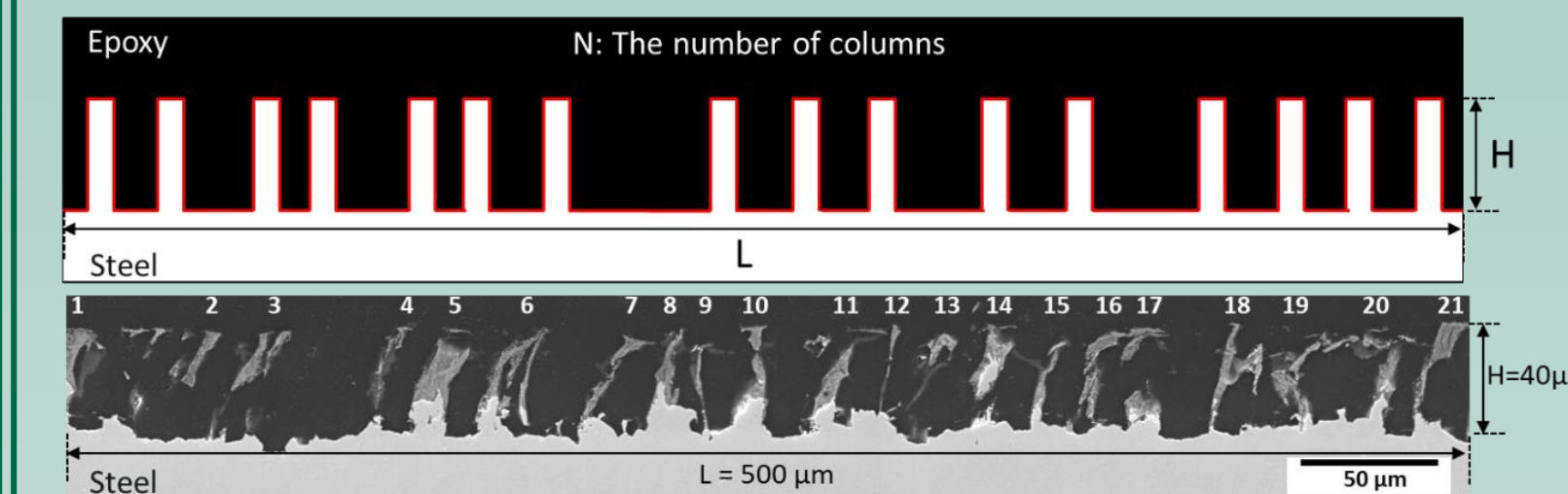
$$R = \frac{\text{Cathodic area with Fe}_3\text{C}}{\text{Cathodic area without Fe}_3\text{C}} = \frac{i_{lim, with Fe_3C}}{i_{lim, without Fe_3C}} \approx 4.0$$



- After normalization, cathodic reaction was retarded to the same extent as that on bare surface as well.
- The lesser retardation of the cathodic reaction reflected in the polarization curve was only due to the additional cathodic area by residual cementite.

### Cathodic Area Ratio Verification

**Method:** The ratio of cathodic reaction area with and without residual cementite was estimated from cross-sectional SEM images.



$$R = \frac{\text{Cathodic area with Fe}_3\text{C}}{\text{Cathodic area without Fe}_3\text{C}} \approx \frac{\text{Perimeter of the red line}}{L} = \frac{2 * N * H + L}{L} \approx 3.85 \pm 0.52$$

## Conclusions

- Residual cementite harmed inhibition efficiency due to galvanic coupling effects *via* serving as an additional cathodic area.
- Both anodic and cathodic reactions can be inhibited equally as on bare steel.
- The lesser retardation of the cathodic reaction reflected in the polarization curve was only due to the additional cathodic area.
- The minimum inhibited corrosion rate with residual cementite was always larger than that on bare steel.

## Limitation & Future Work

**Limitation:** Bulk concentration of CI decreased in this close system due to adsorption at different interfaces.

### Future work:

- Continuously inject CI for long-term exposure to simulate CI injection in pipelines.
- Study this effect using different types of CIs and steels (different carbon contents and microstructures).

## References

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