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Corrigendum

Corrigendum to "A correlation for interfacial area concentration in high void fraction flows in large diameter channels" [Chem. Eng. Sci. 131 (2015) 172 - 186



J.P. Schlegel ^{a,*}, T. Hibiki ^b

There is a typographical mistake in Eq. (21), used in the derivation of the final model, which should read

$$v_{r1} = \sqrt{2} \left(\frac{\sigma g \Delta \rho}{\rho_f^2} \right)^{1/4} (1 - \alpha_1)^{3/4}$$
 (21)

This typographical mistake is also present in Eq. (22b), which is necessary for implementation of the final model, which should

$$f(\alpha) \equiv \left(\left(\frac{8}{3} \right)^{1/3} (1 - \alpha_2)^{2/3} + \frac{\sqrt{2}(1 - \alpha_1)^{3/4}}{3(1 - \alpha_2)^{1/2}} - 1 \right) \tag{22b}$$

These are typographic errors and do not affect the results presented in the original article.

The final correlation of the interfacial area concentration is shown in Table 1.

The authors would like to apologize for this oversight.

Table 1 Final correlation of interfacial area concentration.

Parameter	Recommended formulation
Total interfacial area concentration	$\langle a_i \rangle = \langle a_{i1} \rangle + \langle a_{i2} \rangle$
Group-1 (small bubbles) interfacial area concentration	$\langle a_{i1} angle = rac{6\langlelpha_1 angle}{D_{8m1}}$
Group-2 (slug/churn bubbles) interfacial area concentration	$\langle a_{i2} \rangle = rac{6\langle a_2 angle}{D_{8m2}}$
Sauter mean diameter for Group-1 bubbles	$N_{DSm1} = \frac{D_{Sm.1}}{D_{Sm.2}} = \frac{C_2 \alpha_1 \left[1.13 C_1 \alpha_1^{2/3} \alpha_2 N_{sr} + 0.238 \left(1.39 (1 - \alpha_2)^{2/3} + \frac{\sqrt{2} (1 - \alpha_1)^{3/4}}{3.0 (1 - \alpha_2)^{1/2}} - 1 \right) \right]}{\left[2.44 C_1 (1 - \alpha) N_{sr} + 0.00362 N_{tot}^{2/2} \left(\frac{\rho f}{\rho g} \right) \right]}.$
	$N_{vr} = \frac{\langle \varepsilon \rangle^{1/3} Lo^{1/3}}{v_{c2}}, \ N_{We} = \frac{\rho_f v_{f2}^2 D_H}{\sigma}, \ C_1 = 0.120, \ C_2 = 2.30$
Sauter mean diameter for Group-2 bubbles	$\frac{D_{Sm2}}{D_h} = \frac{C_3 N_{we}^{-1}}{0.238 N_{sr} (1 + \alpha_1 \alpha_2 - \alpha) + 0.996 \alpha_1 \left(1.39 (1 - \alpha_2)^{2/3} + \frac{\sqrt{2} (1 - \alpha_1)^{3/4}}{3.0 (1 - \alpha_2)^{1/2}} - 1\right)}$
	$C_3 = 8.55$
Turbulence dissipation	$\langle arepsilon angle = \langle arepsilon_{sh} angle + \langle arepsilon_{BI} angle pprox rac{0.316}{Re_m^{0.25}} rac{arepsilon_m^3}{2D_H} + \left\langle j_g ight angle \! g$
	$N_{\mathrm{Re}_m} = rac{ ho_m u_m \mathrm{D}_H}{\mu_f} rac{1}{1-\langle lpha angle}, \; ho_m = ho_g \langle lpha angle + ho_f (1-\langle lpha angle), \; u_m = rac{ ho_g \langle j_g angle + ho_f \langle j_f angle}{ ho_m}$
Group-1 void fraction	$\langle lpha_1 angle = \left\langle lpha_{ m gs} ight angle rac{1 - \langle lpha_{ m sc} angle}{1 - \left\langle lpha_{ m sc} ight angle}$
	$\langle lpha_{gs} \rangle = \min \{ \langle lpha \rangle \ , \ 0.63 tanh(0.00145 N_{Re_s} \langle lpha \rangle) \}$
	$N_{Re_{\scriptscriptstyle E}} = rac{\langle arepsilon angle^{1/3} L a^{4/3}}{v_{ m f}}, \ La = \sqrt{rac{\sigma}{\Delta ho m g}}$
Group-2 void fraction	$\langle \alpha_2 \rangle = 1 - \langle \alpha_1 \rangle$

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