



## MATHEMATICAL MODEL OF ELECTROCATALYSIS OF METHANOL OXIDATION AT THE MIXTURE OF NANOCRYSTALS OF PLATINUM AND RUTHENIUM DIOXIDE

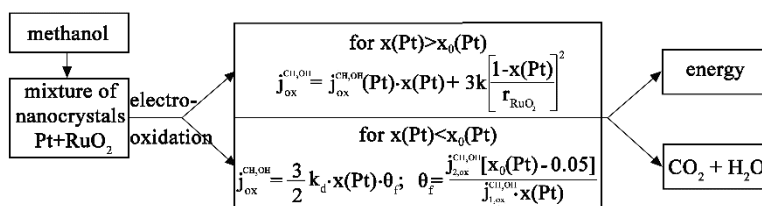
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Mathematical model representing a catalytic effect of a nanocrystal mixture of metallic platinum and ruthenium dioxide for electrooxidation of methanol is established. Dependence of a current density of the methanol electrooxidation on the chemical composition and size of nanocrystals is determined in the model. A good agreement between theoretical values and experimental results corroborates that electrooxidation of methanol is guided by a bifunctional mechanism. The model is based on the fact that the catalytic effect is proportional to the length of the contact border between nanocrystals of metallic platinum and nanocrystals of ruthenium dioxide. Ru-OH particles are formed on the Ru atoms at the border of crystal grains, at potentials more negative than on platinum. These species oxidize firmly bound intermediates CO<sub>ad</sub> located on the adjacent Pt atoms and thus release the Pt atoms for adsorption and dehydrogenation of subsequent molecules of methanol.



### INTRODUCTION

In the last couple of decades, research of many scientific groups has been focused on development of renewable energies, i.e. fuel cells, particularly direct liquid-feed fuel cells. The use of hydrogen in fuel cells is unfavorable due to high costs of miniaturized storage containers and potential danger during its application and transportation. Additionally, low gas-phase energy density of hydrogen also limits its use in fuel cells.<sup>1</sup> Thus, major research studies have been targeted towards finding an appropriate replacement for hydrogen. To this end, hydrogen was substituted with small organic molecules, such as methanol, formaldehyde, formic acid, 1- and 2-propanol in the liquid

fuel cells. Unlike gaseous cells, the liquid fuel cells have a high theoretical energy density (~ 9 kWh kg<sup>-1</sup>) and are easy to handle, transport and distribute.<sup>2</sup> Therefore, a lot of efforts have been put into development of direct simple organic molecules fuel cells as potential power sources for portable electronic devices (mobile phones, lap tops, digital cameras etc.).<sup>3,4</sup>

Oxidation of simple organic molecules begins with their adsorption on the surface of the most investigated catalyst, Pt. Then, the adsorbed organic molecules are subjected to dehydrogenation, thus producing different intermediates. These intermediates can be strongly and weakly adsorbed.<sup>2, 5–21</sup> The CO<sub>ad</sub> species are strongly

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adsorbed on the surface of the most effective catalyst, Pt.<sup>2, 5-25</sup> Besides CO<sub>ad</sub>, strongly adsorbed COH<sub>ad</sub> species, which block the surface of Pt and prevent further oxidation of subsequent organic molecules, are also formed.<sup>22-25</sup> Hence, the Pt catalyst shows a low activity towards the electrooxidation of small organic molecules. Due to high costs and low durability, extensive studies have been done on platinum-based electrocatalysts (Pt/Sn, Pt/Ti, Pt/Mn, Pt/Co, Pt/Fe, Pt/Bi, Pt/Ni, Pt/Ru and Pt/RuO<sub>2</sub>) for fuel cell applications.<sup>5-8, 24-50</sup> The research conducted in last three decades showed the best catalytic performance of Pt/Ru and Pt/RuO<sub>2</sub> catalysts in the particular application.<sup>5-8, 24, 25, 32-41</sup> The catalytic effect of these catalysts was attributed to both bifunctional mechanism and electronic effect. The leading effect was the bifunctional mechanism, in which the oxy species were formed on Ru atoms at more negative potentials than on Pt atoms. These oxy species strongly oxidize some weakly adsorbed intermediates, bound to adjacent Pt atoms, releasing the Pt atoms and allowing for dehydrogenation of the subsequent organic molecules.<sup>5-8, 24, 25, 32-41</sup> The electronic effect is caused by shifting of the d-band center of Pt in Pt/Ru alloys away from the Fermi level.<sup>32, 33, 36, 41, 51-54</sup> M. Wakisaka *et al.* have studied electronic structures of pure Pt and Pt/Ru alloy electrodes by combining XPS with an electrochemical cell.<sup>51</sup> They have shown that alloying with Ru caused the positive shift of Pt4f<sub>7/2</sub>. A linear relationship between the core level shifts and the CO adsorption energy and thus, weaker adsorption of CO on Pt/Ru have been found. P. Waszeruk *et al.* and C. Lui *et al.* have determined a definite contribution of the electronic effect to the total enhancement of CO<sub>ad</sub> oxidation on Pt/Ru as compared to pure Pt, which was only one-fourth of that of the bifunctional mechanism.<sup>53, 54</sup> M.A. Rigsby *et al.* have examined the effect of the electronic structure of Pt/Ru alloy nanoparticles on reactivity of small organic molecules by combining synchrotron radiation photoelectron spectroscopy and electrochemistry.<sup>52</sup> They have found a linear increase in Pt core-level binding energies with addition of Ru. This behavior was attributed to the lattice strain and charge transfer. Also, it has been found that the bifunctional mechanism contributed more significantly than the electronic effect. R. D. Rolison *et al.* have discovered that hydrous Pt/Ru catalysts were more efficient than Pt/Ru alloys, indicating the significance of Ru-OH species in the mechanism of methanol oxidation.<sup>55, 56</sup> R. P. L. Profeti *et al.* have synthesized uniform films Pt<sub>x</sub>Ru<sub>(1-x)</sub>O<sub>y</sub> with controlled

stoichiometry, a high surface area, good chemical stability and uniform composition throughout the film by thermal decomposition of polymeric precursors. The highest catalytic activity was obtained with the catalyst Pt<sub>0.6</sub>Ru<sub>0.4</sub>O<sub>y</sub>. The catalytic effect of the Pt<sub>x</sub>Ru<sub>(1-x)</sub>O<sub>y</sub> catalysts on methanol oxidation was a result of the existence of amorphous and hydrated RuO<sub>2</sub> and its ability to donate OH species. These OH species promoted the oxidation of CO<sub>ad</sub> to CO<sub>2</sub>. A. A. Belmesov *et al.* have applied Pt particles of the average size of 5 to 7 nm on the Ti<sub>(1-x)</sub>Ru<sub>x</sub>O<sub>2-δ</sub> support.<sup>47</sup> The tolerance of the catalyst towards CO has been found to be dependable on the crystal structure of the support. A higher rate of CO oxidation was obtained with the support with the rutile structure than the support with the anatase structure. When using the catalysts Pt/Ti<sub>(1-x)</sub>Ru<sub>x</sub>O<sub>2-δ</sub> with supports with both rutile and anatase structures, the potential of the onset of CO oxidation decreased with increasing the concentration of RuO<sub>2</sub>.

M. Spasojevic *et al.* have prepared the catalytic coating composed of the mixture of nanocrystals of metallic Pt and RuO<sub>2</sub> of the rutile structure by the thermal procedure on a Ti substrate and used it for the oxidation of CH<sub>3</sub>OH, CH<sub>2</sub>O, HCOOH, CH<sub>3</sub>-CH<sub>2</sub>-CH<sub>2</sub>OH and CH<sub>3</sub>-CHOH-CH<sub>3</sub>.<sup>24, 25, 37-40</sup> It has been found that an increase in the RuO<sub>2</sub> content resulted in the increase in the catalytic activity up to maximum value and its subsequent decrease. The organic molecule oxidation on the coatings with the RuO<sub>2</sub> content higher than optimal was determined by dehydrogenation, whereas the oxidation of strongly bound intermediates, CO<sub>ad</sub>, with oxy species adsorbed on Ru atoms determined the organic molecules oxidation on the coatings with the RuO<sub>2</sub> content lower than optimal. The catalytic effect was a result of the bifunctional mechanism, in which the oxy species were formed on Ru in the rutile structure of RuO<sub>2</sub> at more negative potentials than on pure platinum. These oxy species oxidized intermediates firmly and weakly adsorbed on ensembles of few adjacent Pt atoms at the metallic nanocrystals surface.

This study is aimed to create a mathematical model to predict the catalytic effect of the mixture of nanocrystals of metallic Pt and RuO<sub>2</sub> of rutile structure on the electrooxidation of methanol. The mathematical model is used to determine the nature of catalytic effect, which would allow for designing the optimal chemical composition and microstruc-

ture of Pt/RuO<sub>2</sub> catalyst for the oxidation of simple organic molecules.

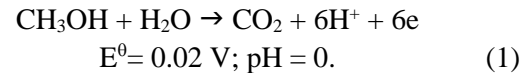
## RESULTS AND DISCUSSION

The thermal procedure is used to form an active catalytic coating, composed of the mixture of nanocrystals of metallic Pt and RuO<sub>2</sub> of the rutile structure, on the titanium substrate, applied in electrochemical oxidation of small organic molecules.<sup>24, 25, 37-40</sup> M. Spasojevic *et al.* have determined the effect of both the mean crystals size and experimental coating composition on the nominal coating composition using the XRD analysis, as shown in Fig. 1.<sup>38</sup>

With increasing the RuO<sub>2</sub> content in the active mixture, the mean crystal size of RuO<sub>2</sub> increases, whereas the mean crystal size of Pt decreases.<sup>38</sup> Experimental molar percentages of Pt are always somewhat lower than nominal. This difference is more pronounced at higher contents of Pt in the solution, applied on the Ti substrate. Previous research have shown that the RuO<sub>2</sub> content affected the catalytic activity of the coating in the electrooxidation of CH<sub>3</sub>OH, CH<sub>2</sub>O, HCOOH, CH<sub>3</sub>-CH<sub>2</sub>-CH<sub>2</sub>OH and CH<sub>3</sub>-CHOH-CH<sub>3</sub>.<sup>24, 37-40</sup> With increasing the RuO<sub>2</sub> content, the catalytic activity increased, reached its maximum and then decreased. The catalytic effect of the mixture of nanocrystals of metallic Pt and RuO<sub>2</sub> of the rutile structure has been attributed to the bifunctional

mechanism.<sup>24, 37-40</sup> In order to corroborate the bifunctional mechanism, a mathematical model of the catalytic effect of the mixture of nanocrystals of Pt and RuO<sub>2</sub> on the methanol oxidation is set.

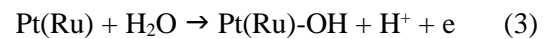
The overall oxidation of methanol in acid fuel cells is a 6-electron process which proceeds as follows:



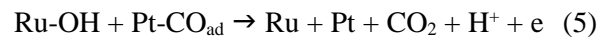
Electrooxidation of CH<sub>3</sub>OH is a multi-step process. Prior to CO<sub>ad</sub> development at the electrode, there are four consecutive single-electron stages:



Then CO<sub>ad</sub> is oxidized by the oxy species formed on Pt or Ru:



The oxy species formed on Ru at more negative potentials than on Pt, oxidize adsorbed CO<sub>ad</sub> on the adjacent Pt atoms at more negative potentials.



The released Ru atoms can react with new OH species arriving from adjacent Ru atoms by surface diffusion, or the discharged Ru atoms can participate in reaction (2) and form new OH<sub>ad</sub> species.

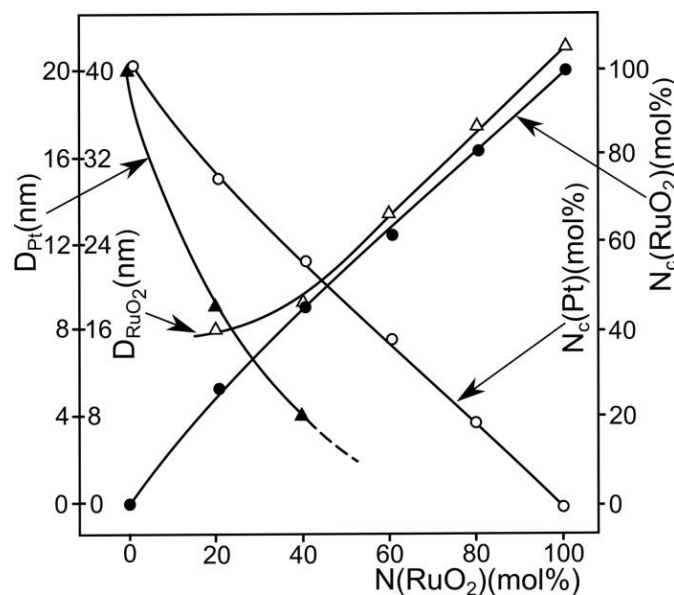


Fig. 1 – The content of (○) Pt (N<sub>c</sub>(Pt)), and (●) RuO<sub>2</sub> (N<sub>c</sub>(RuO<sub>2</sub>)) in the coating and the mean crystals size of (▲) Pt (D(Pt)) and (△) RuO<sub>2</sub> (D(RuO<sub>2</sub>)) as a function of the nominal coating composition, N(RuO<sub>2</sub>).

Simultaneously, at released Pt atoms  $\text{CO}_{\text{ad}}$  species are reformed by dehydrogenation of  $\text{CH}_3\text{OH}$  or by coming of new CO species from adjacent Pt atoms by rapid diffusion.

Reactions (1)–(4) compose a main reaction pathway of  $\text{CH}_3\text{OH}$  oxidation. However, side reactions also occur simultaneously with the main pathway. The rates of these side reactions are negligible compared to the rate of the main reaction pathway.<sup>24, 25, 37–40</sup>

The following assumptions are made prior to setting the mathematical model:

1. The catalytic effect is a result of  $\text{CO}_{\text{ad}}$  oxidation on Pt atoms with Ru-OH species located on the contact edge of  $\text{RuO}_2$  nanocrystals.<sup>24, 25, 37–40</sup>
2. Surface diffusion of the firmly bound intermediates  $\text{CO}_{\text{ad}}$  over the surface of Pt nanocrystals to the grain border is a rapid process.<sup>57</sup>
3. Diffusion of OH species over the surface of  $\text{RuO}_2$  nanocrystals to Ru atoms at the grain border and reaction of RuOH species formation from  $\text{H}_2\text{O}$  molecules are rapid processes.<sup>24, 25, 37–40, 57–59</sup>

These assumptions indicate the increase in the rate of oxidation of the firmly bound intermediate  $\text{CO}_{\text{ad}}$  with rising the size of the contact border between nanocrystals of Pt and  $\text{RuO}_2$ . The increase in the contact border results in rise in the rate of methanol oxidation until the rates of dehydrogenation and  $\text{CO}_{\text{ad}}$  oxidation equalize. After the rates equalization, the increase in the  $\text{RuO}_2$  content declines the catalytic effect due to lower number of ensembles of Pt atoms, required for adsorption and dehydrogenation of  $\text{CH}_3\text{OH}$ .

When the content of  $\text{RuO}_2$  is lower than that of Pt, it can be assumed that the  $\text{RuO}_2$  nanocrystals are completely surrounded by the Pt nanocrystals. The contact border length between the nanocrystals of Pt and  $\text{RuO}_2$  is equal to that of  $\text{RuO}_2$  nanocrystals. It is assumed that the average surface of nanocrystals is of circular shape and the radius of the average size of  $\text{RuO}_2$  nanocrystals,  $r_{\text{RuO}_2}$  is approximately equal to  $\frac{1}{2} D_{\text{RuO}_2}$ . The length of the contact border of one  $\text{RuO}_2$  nanocrystal, surrounded by the Pt nanocrystals is:

$$j_{\text{ox}}^{\text{CO}}(\text{Pt}/\text{RuO}_2) = k_{\text{ox}}^{\text{Pt}/\text{RuO}_2} \cdot c(\text{RuOH}) \cdot c(\text{CO}) \cdot 4 \cdot F_{\text{R}} \left[ \frac{(1-x(\text{Pt}))}{r_{\text{RuO}_2}} \right]^2 \quad (11)$$

where:  $k_{\text{ox}}^{\text{Pt}/\text{RuO}_2}$  – the rate constant of the reaction (11),  $c(\text{RuOH})$  – the linear concentration of the RuOH species at the contact border and  $c(\text{CO})$  – the linear concentration of the  $\text{CO}_{\text{ad}}$  intermediate at the

$$l = 2 \cdot r_{\text{RuO}_2} \pi \quad (6)$$

where:  $l$  – perimeter of  $\text{RuO}_2$  nanocrystal and  $r_{\text{RuO}_2}$  – radius of the average size of  $\text{RuO}_2$  nanocrystals.

The number of  $\text{RuO}_2$  species,  $n_{\text{RuO}_2}$ , at the real surface of an electrode is determined by the equation:

$$n_{\text{RuO}_2} = \frac{S \cdot (1-x(\text{Pt}))}{r_{\text{RuO}_2}^2 \pi} \quad (7)$$

where:  $n_{\text{RuO}_2}$  – the number of  $\text{RuO}_2$  nanocrystals at the real surface of the electrode,  $S$  – the real surface of the electrode and  $x = 0.01\text{Nc}(\text{Pt})$  – mola fraction of the Pt in the coating. The total length of the contact edges,  $L$ , between Pt and  $\text{RuO}_2$  nanocrystals is:

$$L_{\text{Ru}} = n_{\text{RuO}_2} \cdot 2r_{\text{RuO}_2} \pi = \frac{2 \cdot S \cdot (1-x(\text{Pt}))}{r_{\text{RuO}_2}} \quad (8)$$

The real surface is determined by the equation:

$$S = S_{\text{G}} \cdot F_{\text{R}} \quad (9)$$

where:  $S_{\text{G}}$  – geometric surface area,  $F_{\text{R}}$  – roughness factor. The roughness factor used in this paper is independent of the chemical composition.<sup>38</sup>

At higher Pt contents, the slowest step in the oxidation of small organic molecules is the reaction of oxidation of firmly bound intermediates with adsorbed OH species. The total current density of the oxidation of  $\text{CO}_{\text{ad}}$ ,  $j_{\text{u,ox}}^{\text{CO}}$ , is determined by the following equation:

$$j_{\text{u,ox}}^{\text{CO}} = j_{\text{ox}}^{\text{CO}}(\text{Pt}) \cdot x(\text{Pt}) + j_{\text{ox}}^{\text{CO}}(\text{Pt}/\text{RuO}_2) \quad (10)$$

where:  $j_{\text{u,ox}}^{\text{CO}}$  – the total current density of  $\text{CO}_{\text{ad}}$  oxidation,  $j_{\text{ox}}^{\text{CO}}(\text{Pt})$  – the current density of oxidation at pure Pt,  $j_{\text{ox}}^{\text{CO}}(\text{Pt}/\text{RuO}_2)$  – the current density of oxidation caused by the catalytic effect of the nanocrystals mixture.

With increasing the size of the contact border, the number of RuOH species and firmly adsorbed intermediates rises linearly at that border, thus:

contact border. The linear concentration of RuOH is proportional to the degree of coverage of Ru atoms with OH species:

$$c(\text{RuOH}) = k(\text{RuOH}) \cdot \theta(\text{RuOH}) \quad (12)$$

The reaction of RuOH formation (3) and surface diffusion of the  $\text{OH}_{\text{ad}}$  species over  $\text{RuO}_2$  crystals to their edge are substantially more rapid processes than reaction (5).<sup>24,25,37-40,57-59</sup> Therefore,  $\theta(\text{RuOH})$  and  $c(\text{RuOH})$  are constants at the given potential. Thus:

$$c(\text{RuOH}) = k'(\text{RuOH}) \quad (13)$$

where:

$$k'(\text{RuOH}) = k(\text{RuOH}) \cdot \theta(\text{RuOH}) \quad (14)$$

The linear concentration of the intermediate  $\text{CO}_{\text{ad}}$  at the contact borders of Pt nanocrystals is proportional to the coverage degree of the Pt surface with  $\text{CO}_{\text{ad}}$ :

$$c(\text{CO}_{\text{ad}}) = k(\text{CO}) \cdot \theta(\text{CO}_{\text{ad}}) \quad (15)$$

when both reaction of  $\text{CH}_3\text{OH}$  dehydrogenation and the surface diffusion of  $\text{CO}_{\text{ad}}$  over the Pt crystals are more rapid processes than the oxidation of the intermediate  $\text{CO}_{\text{ad}}$ , then  $\theta(\text{CO}_{\text{ad}})$  and  $c(\text{CO}_{\text{ad}})$  are constants at given potential.<sup>24,25,37-40,57-59</sup> Therefore:

$$c(\text{CO}_{\text{ad}}) = k'(\text{CO}) \quad (16)$$

where:

$$k'(\text{CO}) = k(\text{CO}) \cdot \theta(\text{CO}_{\text{ad}}) \quad (17)$$

By introducing a new constant  $k$ , determined by the equation:

$$k = 4 \cdot F_R k_{\text{ox}}^{\text{Pt}/\text{RuO}_2} \cdot k'(\text{RuOH}) \cdot k'(\text{CO}) \quad (18)$$

the total current density of  $\text{CO}_{\text{ad}}$  oxidation is expressed as:

$$j_{\text{u,ox}}^{\text{CO}} = j_{\text{ox}}^{\text{CO}}(\text{Pt}) \cdot x(\text{Pt}) + k \cdot \left[ \frac{1-x(\text{Pt})}{r_{\text{RuO}_2}} \right]^2 \quad (19)$$

From equations (1)-(5), the current density of  $\text{CH}_3\text{OH}$  oxidation is:

$$j_{\text{ox}}^{\text{CH}_3\text{OH}} = j_{\text{u,d}}^{\text{CH}_3\text{OH}} + j_{\text{u,ox}}^{\text{CO}} \quad (20)$$

and:

$$j_{\text{u,d}}^{\text{CH}_3\text{OH}} = 2 \cdot j_{\text{u,ox}}^{\text{CO}} \quad (21)$$

where:  $j_{\text{ox}}^{\text{CH}_3\text{OH}}$  – the current density of  $\text{CH}_3\text{OH}$  oxidation and  $j_{\text{u,d}}^{\text{CH}_3\text{OH}}$  – the total current density of dehydrogenation.

The equation for the current density of oxidation is obtained by combining equations (19), (20) and (21):

$$j_{\text{ox}}^{\text{CH}_3\text{OH}} = j_{\text{ox}}^{\text{CH}_3\text{OH}}(\text{Pt}) \cdot x(\text{Pt}) + 3 \cdot k \left[ \frac{1-x(\text{Pt})}{r_{\text{RuO}_2}} \right]^2 \quad (22)$$

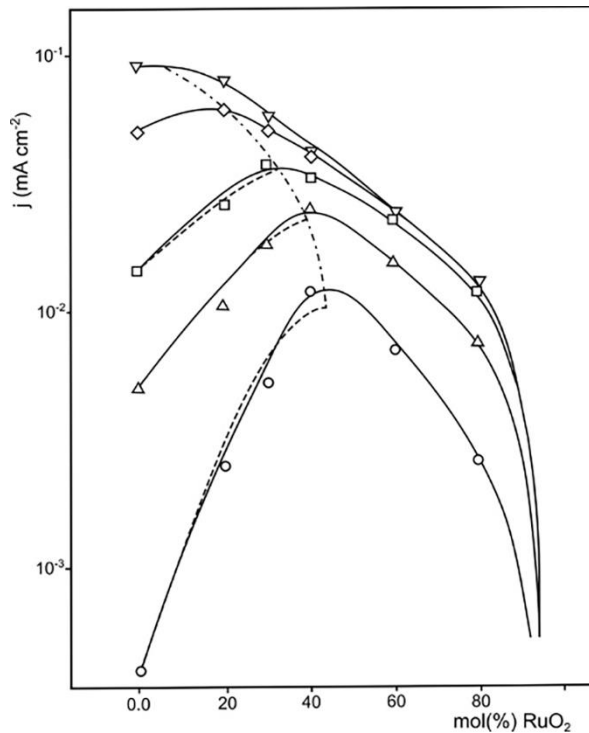


Fig. 2 – The current density of  $\text{CH}_3\text{OH}$  oxidation as a function of the content and coating potentials. Experimental values: (O) 0.517 V; ( $\Delta$ ) 0.550 V; ( $\square$ ) 0.583 V; ( $\diamond$ ) 0.633 V; ( $\nabla$ ) 0.667 V. The current density values were recorded after holding the anode for 3 min at 0.049 V and 30 min at desired potential (solution:  $0.5 \text{ mol dm}^{-3} \text{H}_2\text{SO}_4 + 0.25 \text{ mol dm}^{-3} \text{CH}_3\text{OH}$ ;  $t = 25 \text{ }^\circ\text{C}$ ). The curves presented with dashed lines are obtained from the equation (22). The dash-dotted curve presents dependence of the maximum of current density on potential.

Fig. 2 shows dependence of the current density of CH<sub>3</sub>OH oxidation on the potential and active coating content, obtained either experimentally or theoretically by applying equation (22).

Fig. 1 shows that the increase in the RuO<sub>2</sub> content results in rise in the catalytic activity, which reaches the maximum value at a certain composition of the coating. Subsequent increase of the RuO<sub>2</sub> content declines the catalytic activity. At the RuO<sub>2</sub> contents lower than maximal, the rate of methanol oxidation is determined by the slow reaction of oxidation of the firmly bound intermediate CO<sub>ad</sub>. With increasing the RuO<sub>2</sub> content, the oxidation of CO<sub>ad</sub> accelerates (reaction (5)) due to increase in the length of the contact edge between nanocrystals of Pt and RuO<sub>2</sub>. Simultaneously, the rate of CH<sub>3</sub>OH dehydrogenation (reaction (2)) declines as a result of decrease in the surface of Pt nanocrystals and hence, the number of ensembles of adjacent Pt atoms. At the certain RuO<sub>2</sub> concentration, when rates of these two reactions equalize, the maximum catalytic effect of the coating is accomplished.<sup>38</sup> As shown in Fig. 2, with decreasing the potential below 0.67 V, the RuO<sub>2</sub> content shifts to the higher values for the maximum catalytic activity of the coating. At the coatings with more than the optimal amount of RuO<sub>2</sub>, the rate of methanol oxidation is determined by the CH<sub>3</sub>OH dehydrogenation. A high coverage degree of Ru atoms with oxy species, which are formed at more negative

potentials than on Pt, results in more comprehensive oxidation of CO<sub>ad</sub> on the Pt/RuO<sub>2</sub> coating at potentials more negative than 0.67 V than on pure Pt.<sup>25, 38</sup> As a consequence, the coverage degree of Pt atoms of the active coating with the firmly adsorbed CO<sub>ad</sub> species rapidly declines at more negative potentials than on pure Pt.<sup>25, 38</sup>

By fitting the equation (22) with experimentally obtained dependences, shown in Fig. 1, the values of the constant *k* at different potentials are determined. Subsequently, these values and experimental results from Fig. 1 are used to calculate the theoretical values of  $j_{ox}^{CH_3OH}$ . Good agreement between the theoretically obtained and experimental values (Fig. 2) indicates validity of the proposed mechanism of the CH<sub>3</sub>OH electrooxidation on the mixture of nanocrystals of Pt and RuO<sub>2</sub>, at the RuO<sub>2</sub> contents lower than optimal.

When the RuO<sub>2</sub> contents are greater than optimal, the current density of oxidation is determined by the reaction of dehydrogenation of CH<sub>3</sub>OH (reaction 2):

$$j_{ox}^{CH_3OH} = \frac{3}{2} \cdot j_{u,d}^{CH_3OH} \quad (23)$$

The total current density of dehydrogenation is proportional to the molar fraction of Pt and its fraction of free surface area  $\theta_f$ :

$$j_{u,d}^{CH_3OH} = k_d \cdot x(Pt) \cdot \theta_f = k_d \cdot x(Pt) \cdot (1 - \theta(CO_{ad})) \quad (24)$$

According to the proposed mechanism, the coverage degree  $\theta(CO_{ad})$  is negligible for the electrode with the Pt content 5 mol% lower than the optimal [ $x_0(Pt) - 0.05$ ], and thus:

$$j_{1,u,d}^{CH_3OH} = k_d \cdot [x_0(Pt) - 0.05] \quad (25)$$

At the same potential, the total current density of dehydrogenation,  $j_{2,u,d}^{CH_3OH}$ , on the coating with  $x(Pt) < x_0(Pt) - 0.05$  is:

$$j_{2,u,d}^{CH_3OH} = k_d \cdot x(Pt) \cdot \theta_f \quad (26)$$

Combination of the equation (23), (25) and (26) results in:

$$\theta_f = \frac{j_{2,u,d}^{CH_3OH} \cdot [x_0(Pt) - 0.05]}{j_{1,u,d}^{CH_3OH} \cdot x(Pt)} = \frac{j_{2,ox}^{CH_3OH} \cdot [x_0(Pt) - 0.05]}{j_{1,ox}^{CH_3OH} \cdot x(Pt)} \quad (27)$$

Using the equation (27) and the experimental data shown in Fig. 2, dependence of  $\theta_f$  on the RuO<sub>2</sub> content and potential is obtained (Fig. 3). As seen in Fig. 3,  $\theta_f \approx 1$  in the RuO<sub>2</sub> content region from

optimal to  $x(RuO_2) = 0.45$ . From  $x(RuO_2) = 0.45$  to  $x(RuO_2) = 0.81$ ,  $\theta_f$  slowly decreases till  $\theta_f = 0.75$ . The change in the RuO<sub>2</sub> content from optimal to  $x(RuO_2) = 0.40$  results in decrease in the average size of Pt nanocrystals to 4 nm (Fig. 1). When Pt nanocrystals are larger than 4 nm, the number of ensembles of adjacent Pt atoms, required for the CH<sub>3</sub>OH adsorption, is proportional to the Pt surface. Therefore,  $\theta_f$  stays constant in this region of the RuO<sub>2</sub> contents. However, the increase in the RuO<sub>2</sub> content from  $x(RuO_2) = 0.45$  to  $x(RuO_2) = 0.81$  results in decline in the average size of nanocrystals to values below 3 nm (Fig. 1). This causes the decrease in the number of ensembles of adjacent Pt atoms, required for the CH<sub>3</sub>OH adsorption, per the surface unit of Pt, resulting in drop of the current density of CH<sub>3</sub>OH dehydrogenation and thus  $\theta_f$ .<sup>60</sup> Therefore,  $\theta_f$  decreases as a consequence of the increased number of Pt atoms at edges and stairs that cannot be included into ensembles of Pt atoms, which adsorb CH<sub>3</sub>OH molecules.<sup>60</sup>

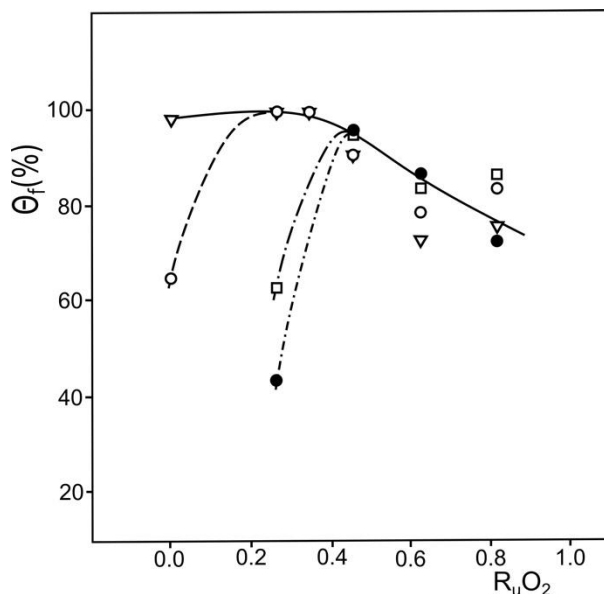


Fig. 3 –  $\theta_f$  as a function of the  $\text{RuO}_2$  content and potential: (▽) 0.667 V; (○) 0.633 V; (□) 0.550 V; (●) 0.517 V (solution:  $0.5 \text{ mol dm}^{-3} \text{ H}_2\text{SO}_4 + 0.25 \text{ mol dm}^{-3} \text{ CH}_3\text{OH}$ ;  $t = 25 \text{ }^\circ\text{C}$ ).

In the region of  $\text{RuO}_2$  contents that are below the optimal value, with decreasing the  $\text{RuO}_2$  content  $\theta_f$  declines (Fig. 3). Here, as a consequence of the decrease in the  $\text{RuO}_2$  content, difference between the rates of  $\text{CH}_3\text{OH}$  dehydrogenation and  $\text{CO}_{\text{ad}}$  oxidation rises, resulting in the increase in the coverage degree of Pt with  $\text{CO}_{\text{ad}}$  and thus, the decline in  $\theta_f$ . The presented figures and theoretical considerations indicate the validity of the proposed mechanism of the catalytic effect of the mixture of Pt and  $\text{RuO}_2$  nanocrystals in the electrooxidation of  $\text{CH}_3\text{OH}$ . Insight in the mechanism of electrocatalytical oxidation of small organic molecules would allow for determination of the optimal composition and microstructure of the Pt/ $\text{RuO}_2$  catalyst and thus, the parameters of its synthesis.

## EXPERIMENTAL

An active coating composed of the mixture of nanocrystals of metallic Pt and  $\text{RuO}_2$  of the rutile structure on a titanium substrate of a surface area of  $3.0 \text{ cm}^2$ , was prepared by the thermal procedure previously described.<sup>38</sup> Briefly, the solutions  $\text{H}_2\text{PtCl}_6$  and  $\text{RuCl}_3$  (Johnson and Matthey) in 2-propanol were spread over the properly prepared surface of titanium plates. After evaporation of the solvent, the titanium plates were heated for 5 minutes at  $500 \text{ }^\circ\text{C}$  in the air atmosphere. The procedure was repeated five times until the coating depth of  $1.2 \text{ mgcm}^{-2}$  based on the pure metals was achieved. After spreading of the last layer, the electrodes were heated for 45 minutes at  $500 \text{ }^\circ\text{C}$ .

The chemical composition of the layer was determined by electronic dispersion spectroscopy, EDS (QX3000 spectrometer).

A Phillips PW1730 diffractometer with a vertical goniometer PW 1050 and a static non-rotating sample carrier

was used for X-ray diffraction analyses. This had a 35 kV, 20 mA power supply for copper excitation, and an AMR graphite monochromator. Phases were identified by reference to ASTM tables.

The electrochemical measurements were carried out with the usual electrical set-up consisting of a potentiostat equipped with a programmer (Potentiostat-Galvanostat model 173, EGG Princeton, Applied Research, Princeton, USA), an x-y recorder (Hewlett Packard 7035 B) and a digital voltmeter (Pros Kit 03-9303 C). The experiments were conducted in a standard electrochemical cell with a separate part for the saturated mercury sulphate electrode and Luggin capillary. The counter electrode was a flat platinum mesh with a geometric surface area of  $16 \text{ cm}^2$  placed parallel to the working electrode. The cell was placed in the thermostat. The operating temperature was  $25 \pm 0.5 \text{ }^\circ\text{C}$ . The solutions were made from p.a. chemicals (Merc) and demineralized water. Prior to the electrochemical measurements, oxygen was removed from the solution by the introduction of nitrogen that was firstly purified by passing over molecular sieves and copper shavings. All potentials were expressed relative to the standard hydrogen electrode. The potentials were corrected for the ohmic potential drop, which was determined by the galvanostatic pulse method. The current density values were recorded after holding the electrode for 3.0 min at 0.049 V and 30.0 min at desired potential. When the electrode was kept at desired potential, the initial value of current decreases instantly to substantially lower value after 30.0 min, and remains approximately constant following 60 min.

## CONCLUSIONS

In this paper, the mathematical model of the effect of the chemical composition of the Pt/ $\text{RuO}_2$  coating on its catalytic activity in the electrooxidation of methanol is set. The coating is formed by the thermal procedure and composed of the mixture of

nanocrystals of metallic Pt and RuO<sub>2</sub> of the rutile structure. The correlation between the chemical composition and size of nanocrystals as well as the current density of electrooxidation of methanol at different potentials is established. Good agreement between experimental and theoretical values indicates the validity of the proposed bifunctional mechanism in catalyze of the methanol electrooxidation reaction. The mathematical model shows that the increase in the RuO<sub>2</sub> content causes the rise in the catalytic activity up to the maximum value and then its decrease. This model corroborates that the increase in the catalytic activity with rising the RuO<sub>2</sub> content up to optimal value is caused by the increase in the length of a contact border between nanocrystals of metallic Pt and RuO<sub>2</sub>. Ru-OH species are formed on the Ru atoms at the border of nanocrystals, at potentials more negative than on metallic Pt. These oxy species oxidize firmly bound intermediates CO<sub>ad</sub>, located on adjacent Pt atoms and thus, release these Pt atoms for adsorption and dehydrogenation of subsequent CH<sub>3</sub>OH molecules. When the RuO<sub>2</sub> content is higher than optimal, the catalytic activity is determined by the reaction of methanol dehydrogenation. In this region, the increase in the RuO<sub>2</sub> content results in decline of the catalytic activity due to the decrease in the Pt surface and thus, the number of ensembles of adjacent Pt atoms required of the methanol adsorption.

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### Nomenclature list

1.  $N_c(Pt)$ , mol% – content of Pt in the coating
2.  $N_c(RuO_2)$ , mol% – content of RuO<sub>2</sub> in the coating
3.  $N(Pt)$ , mol% – nominal content of Pt in the coating
4.  $N(RuO_2)$ , mol% – nominal content of RuO<sub>2</sub> in the coating
5.  $D(Pt)$ , nm – mean crystal size of Pt
6.  $D(RuO_2)$ , nm – mean crystal size of RuO<sub>2</sub>
7.  $E^\theta$ , V – standard electrode potential
8.  $r_{RuO_2}$ , nm – radius of average crystal size of RuO<sub>2</sub>
9.  $r_{Pt}$ , nm – radius of average crystal size of Pt
10.  $x(Pt)$  – mol fraction of Pt in the coating
11.  $S$ , cm<sup>2</sup> – real surface area
12.  $L$ , nm – total length of the contact edge between Pt and RuO<sub>2</sub> nanocrystals
13.  $S_G$ , cm<sup>2</sup> – geometric surface area
14.  $F_R$  – friction factor
15.  $j_{u,ox}^{CO}$ , mA cm<sup>-2</sup> – total current density of the CO<sub>ad</sub> oxidation
16.  $j_{ox}^{CO}(Pt)$ , mA cm<sup>-2</sup> – current density of the CO<sub>ad</sub> oxidation at pure Pt
17.  $j_{ox}^{CO}(Pt/RuO_2)$ , mA cm<sup>-2</sup> – current density of the oxidation caused by the catalytic effect of the nanocrystals mixture
18.  $k_{ox}^{Pt/RuO_2}$ , mA cm<sup>2</sup> mol<sup>-2</sup> – rate constant of the oxidation reaction caused by the catalytic effect of the nanocrystals mixture
19.  $c(RuOH)$ , mol cm<sup>-1</sup> – linear concentration of RuOH at the constant border between nanocrystals Pt and RuO<sub>2</sub>
20.  $\theta(RuOH)$  – coverage degree of Ru with OH<sub>ad</sub> species
21.  $k(RuOH)$ , mol cm<sup>-1</sup> – constant of proportionality between  $c(RuOH)$  and  $\theta(RuOH)$  in the equation (12)
22.  $k'(RuOH)$ , mol cm<sup>-1</sup> – constant in the equation (14)
23.  $c(CO_{ad})$ , mol cm<sup>-1</sup> – linear concentration of CO<sub>ad</sub> at the contact border between nanocrystals Pt and RuO<sub>2</sub>
24.  $k(CO)$ , mol cm<sup>-1</sup> – constant of proportionality between  $c(CO_{ad})$  and  $\theta(CO_{ad})$  in the equation (15)
25.  $\theta(CO_{ad})$  – coverage degree of Pt with CO<sub>ad</sub> species
26.  $k'(CO)$ , mol cm<sup>-1</sup> – constant in the equation (17)
27.  $k$ , mA – constant in the equation (18)
28.  $j_{ox}^{CH_3OH}$ , mA cm<sup>-2</sup> – current density of the CH<sub>3</sub>OH oxidation
29.  $j_{ox}^{CH_3OH}$ , mA cm<sup>-2</sup> – current density of the CH<sub>3</sub>OH oxidation at pure Pt
30.  $j_{u,d}^{CH_3OH}$ , mA cm<sup>-2</sup> – total current density of the CH<sub>3</sub>OH dehydrogenation
31.  $\theta_f$  – fraction of the free Pt surface
32.  $k_d$ , mA cm<sup>-2</sup> – rate constant of the CH<sub>3</sub>OH dehydrogenation
33.  $x_0(Pt)$  – optimal mol fraction of Pt
34.  $j_{1,u,d}^{CH_3OH}$ , mA cm<sup>-2</sup> – total current density of the CH<sub>3</sub>OH dehydrogenation at the coating surface with the composition of  $x_0(Pt) = 0.05$
35.  $j_{2,u,d}^{CH_3OH}$ , mA cm<sup>-2</sup> – total current density of the CH<sub>3</sub>OH dehydrogenation at the coating surface with the composition of  $x(Pt) < x_0(Pt) = 0.05$



36.  $j_{1,ox}^{CH_3OH}$ , mA cm<sup>-2</sup> – current density of the CH<sub>3</sub>OH oxidation at the coating surface with the composition of  $x_0(Pt) = 0.05$
37.  $j_{2,ox}^{CH_3OH}$ , mA cm<sup>-2</sup> – current density of the CH<sub>3</sub>OH oxidation at the coating surface with the composition of  $x(Pt) < x_0(Pt) = 0.05$ .

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