

## Article

# Synthesis, characterization and electrochemical evaluation of anticorrosion property of a tetrapolymer for carbon steel in strong acid media

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## ABSTRACT

A novel tetrapolymer (TP) consisting of carboxylate, sulphonate, phosphonate and sulfur dioxide based comonomers was synthesized using Butler cyclopolymerization technique. The synthesized tetrapolymer was characterized using FTIR, <sup>1</sup>H-NMR, <sup>13</sup>C NMR and elemental analysis. The performance of the tetrapolymer as a corrosion inhibitor for St37 carbon steel in 15% HCl and 15% H<sub>2</sub>SO<sub>4</sub> acid media was assessed using electrochemical impedance spectroscopy (EIS), linear polarization resistance (LPR), potentiodynamic polarization (PDP) and electrochemical frequency modulation (EFM) techniques. The influence of addition of a small amount of KI on the corrosion inhibition efficiency of TP was also assessed. Results obtained showed that the tetrapolymer moderately inhibited the corrosion of St37 steel in the acid media with protection efficiency of 79.5% and 61.1% at the optimum concentration of 1000 mg·L<sup>-1</sup> studied in HCl and H<sub>2</sub>SO<sub>4</sub> media respectively. On addition of 5 mmol·L<sup>-1</sup> KI to the optimum tetrapolymer concentration, the protection efficiency was upgraded to 90.6% and 93.5% in HCl and H<sub>2</sub>SO<sub>4</sub> environment, respectively. The enhanced performance of the polymer in the presence of KI is due to synergistic action deduced from synergism parameter (*S*<sub>1</sub>) which was found to be greater than unity. The tetrapolymer afforded the corrosion inhibition of St37 steel in the acid media by virtue of adsorption of the polymer molecules on the steel surface which was confirmed by ATR-FTIR analysis of the adsorbed film extracted from the steel surface. TP + KI formed complex with St37 steel surface in H<sub>2</sub>SO<sub>4</sub> solution but not in HCl solution.

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## 1. Introduction

In the process of acidizing stimulation or cleanup operations, metal tubulars, down hole tools/valves, surface lines, etc. mainly made of carbon steel are exposed to acidic fluids [1]. The exposure is detrimental to the carbon steel materials as they are prone to corrosion. In addition, metal substrates in high temperature wells experience a drastic increase in corrosion rates. Therefore, controlling corrosion is critical and must be dealt with effectively. In addition, corrosion protection becomes inevitable in order to maintain the integrity and long life of down hole tools installed in an operating oil wells.

Although there are many corrosion protection strategies adopted to control corrosion of metal substrates in diverse corrosive media, the use of corrosion inhibitors for internal pipeline corrosion protection offers the most practical and cost effective method. The key performance

indicators for the selection of corrosion inhibitor include its economic availability, performance (effectiveness to inhibit the metal substrate) and its environmental side effects. Most of the inhibitors for corrosion of steel in acidic media are organic compounds containing nitrogen, oxygen and/or sulfur atoms. The inhibiting action of these compounds is often associated with their ability to adsorb on the metal/solution interface. The use of polymers and polymer composites as corrosion inhibitor for steel in strong acid media can be found in the literature [2–7]. In our laboratory, we have also reported on the use of cyclic cation polymer bearing bis-3-phosphorylpropyl pendants [8] and polypropylene glycol [9] as effective corrosion inhibitors for steel in 15% HCl medium.

Apart from corrosion, there are other problems in the oil and gas industry that required the use of specialty chemicals for treatment. For instance, antiscalants or scale inhibitors are required for scale inhibition, biocides to inhibit the growth of microorganisms/biofouling and demulsifiers or emulsion breakers to separate emulsions, for example water in oil. The use of diverse chemicals simultaneously to treat different problems occurring in the oil field sometimes results in

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the problem of incompatibility. It is highly desirable to have a single compound with dual or multi functions. Previous work has shown that the tetrapolymer acted as an effective antiscalant for  $\text{CaSO}_4$  scale [10]. In order to explore the possibility of tetrapolymer serving a dual purpose as a scale inhibitor and as well as a corrosion inhibitor, the present work reports on the corrosion inhibition performance of tetrapolymer for carbon steel (St37 grade) in 15% HCl and 15%  $\text{H}_2\text{SO}_4$  environments using electrochemical techniques. The effect of the addition of KI on the corrosion inhibition performance of the investigated tetrapolymer was also assessed. Analysis of the adsorbed inhibitor film on the steel surface in comparison with that of the bulk polymer using ATR-FTIR technique was employed to elucidate the mechanism of corrosion inhibition by the tetrapolymer.

## 2. Experimental

### 2.1. Synthesis and characterization of tetrapolymer

The details of the synthesis of the tetrapolymer using Butler cyclopolymerization technique. The polymerization was carried out in a solution of **1** (2.75 g, 15 mmol), **2** (3.83 g, 15 mmol), and **3** (3.29 g, 15 mmol)  $\text{SO}_2$  (2.88 g, 45 mmol) in DMSO (12.5 g) using azobisisobutyronitrile (AIBN) (225 mg) (Scheme 1). The mixture was stirred under  $\text{N}_2$  in a closed RB flask at  $60^\circ\text{C}$  for 48 h. Every 8 h, the flask was opened to release  $\text{N}_2$  generated from the decomposition of AIBN. The reaction mixture became immobile within an hour; at the end of the time elapsed, the reaction mixture was soaked in water, filtered and washed with acetone. The white polymer **4** was then grounded with a mortar and pestle and soaked in methanol, filtered, and dried under vacuum at  $60^\circ\text{C}$  to a constant weight (11.0 g, 90%). The characterization of the obtained tetrapolymer was done using FTIR,  $^{13}\text{C}$  NMR,  $^1\text{H}$  NMR, and elemental analysis. The results from FTIR,  $^{13}\text{C}$  NMR, and elemental analysis can be found in reference [10]. Only  $^1\text{H}$  NMR spectrum is presented herein.

### 2.2. Corrosion inhibition studies

#### 2.2.1. Materials and corrosive media

St37 steel with chemical composition as earlier reported [11] was used as the metal substrate. The corrosive media was 15% HCl and 15%  $\text{H}_2\text{SO}_4$  prepared by diluting analytical reagent grade 37% HCl (Sigma Aldrich) and 98%  $\text{H}_2\text{SO}_4$  (Sigma-Aldrich) with doubled distilled water.

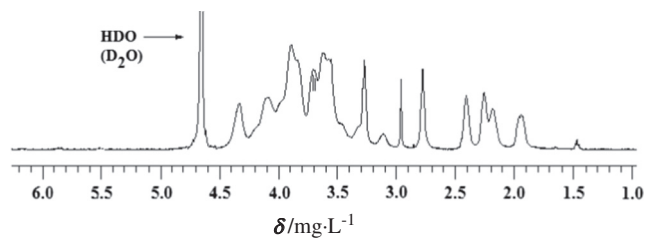
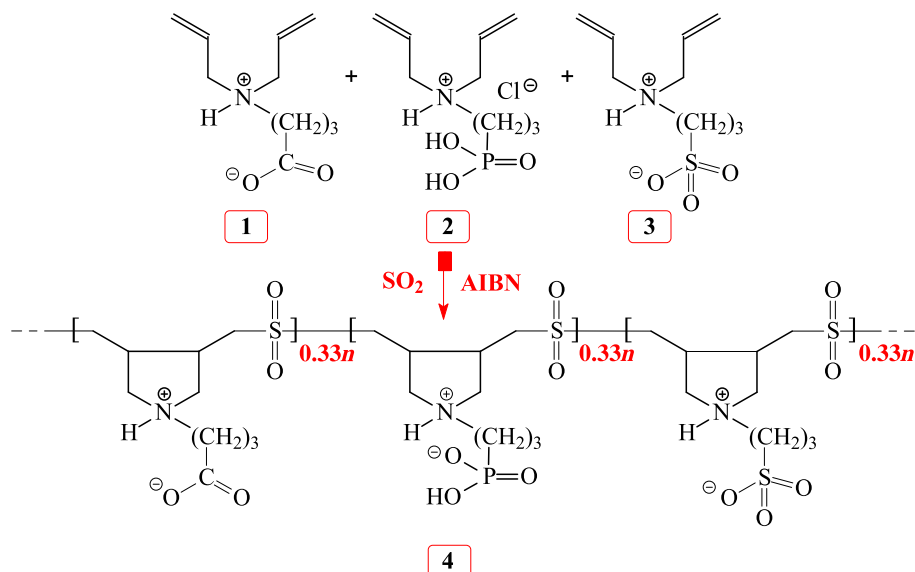


Fig. 1.  $^1\text{H}$  NMR spectrum of tetrapolymer **4** in  $\text{D}_2\text{O}$  in the presence of NaCl.

The synthesized polymer was used as test corrosion inhibitor in the concentration range of  $50\text{--}1000\text{ mg}\cdot\text{L}^{-1}$ . KI (Sigma Aldrich) concentration of  $1\text{ mmol}\cdot\text{L}^{-1}$  and  $5\text{ mmol}\cdot\text{L}^{-1}$  was added to  $1000\text{ mg}\cdot\text{L}^{-1}$  of TP to evaluate the synergistic effect of KI additive.

#### 2.2.2. Electrochemical corrosion tests

Electrochemical corrosion tests were conducted using the Gamry Potentiostat/Galvanostat/ZRA Reference 600 together with Echem analyst software to analyze the experimental data. Conventional three electrode assembly was used to accomplish the electrochemical measurements. The electrodes were made up of St37 steel as working, silver/silver chloride (Ag/AgCl) as reference and graphite rod as the counter electrodes. The working electrode was in the form of a circular disc with an exposed surface area of  $0.75\text{ cm}^2$ . Prior to all electrochemical measurements, the working electrode was immersed for 1 h to ensure that the steady-state open circuit potential (OCP) was established. Potentiodynamic polarization tests were performed at the potential of  $\pm 150\text{ mV}$  from open circuit potential (OCP) at a scan rate of  $0.5\text{ mV}\cdot\text{s}^{-1}$ . LPR experiment was carried out from  $-15$  to  $+15\text{ mV}$  versus OCP at the scan rate of  $0.125\text{ mV}\cdot\text{s}^{-1}$ . Electrochemical impedance spectroscopy (EIS) tests were monitored over the frequency range of  $10^4$  to  $10\text{ mHz}$ , with acquirement of 10 points per decade and a signal amplitude of  $10\text{ mV}$  (peak-to-peak) at  $E_{\text{corr}}$ . EFM measurements were carried using potential perturbation signal with amplitudes of  $10\text{ mV}$ . Measurements were conducted using two frequencies, 2 and 5 Hz. The base frequency was 1 Hz with 32 cycles so the waveform repeats after 1 s. All measurements were repeated at least three times and good reproducibility of the results was observed.



Scheme 1. Synthesis of the tetrapolymer **4**.

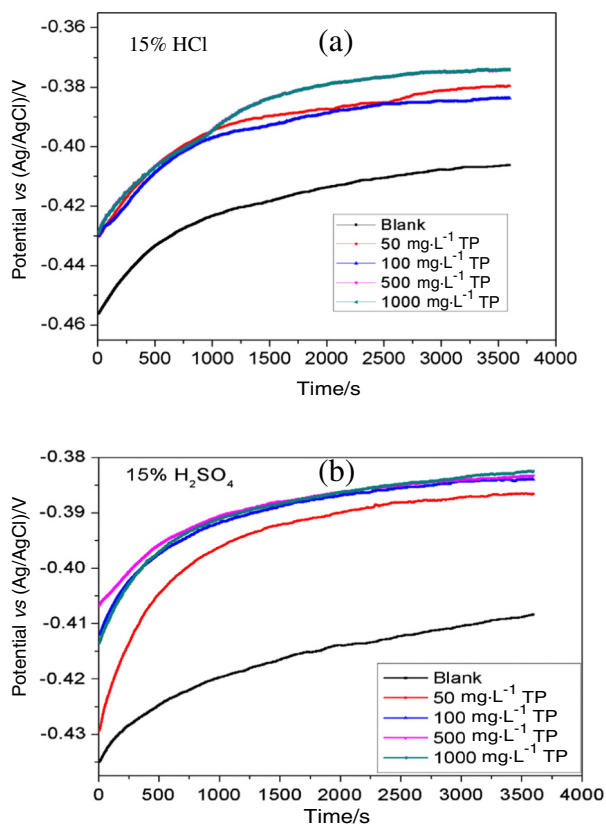


Fig. 2. Variation of OCP with time for St37 steel in (a) 15% H<sub>2</sub>SO<sub>4</sub> and (b) 15% HCl in the absence and presence of different concentrations of TP at 25 °C.

### 2.2.3. Surface analysis

The morphology of the corroded steel surfaces immersed in the corrosive medium in absence and presence of TP and TP in combination of KI were determined using scanning electron microscope (SEM) (JEOL JSM 6610-LV) operated at an acceleration voltage of 20 kV and irradiation current of 10  $\mu$ A.

The UV-Visible spectra were recorded for solutions of 15% HCl and 15% H<sub>2</sub>SO<sub>4</sub> devoid of and containing TP and TP-KI mixtures after 24 h immersion of the carbon steel using JASCO770-UV-Vis spectrophotometer from 250 to 450 nm using a dual beam operated at a resolution of 1 nm with a scan rate of 200 nm·min<sup>-1</sup>.

The ATR-FTIR analysis was performed for pure TP and the films extracted from the carbon steel surface immersed in 15% HCl and 15% H<sub>2</sub>SO<sub>4</sub> containing TP and TP-KI mixtures for 24 h at 25 °C. The ATR-FTIR spectra were recorded in the range of 400–4000 cm<sup>-1</sup> using an IR spectrometry (TA instrument with universal ATR attachment, Nicolet iS5, Thermo Scientific).

## 3. Results and Discussion

### 3.1. Characterization of tetrapolymer (TP)

The <sup>1</sup>H NMR spectrum in D<sub>2</sub>O (Fig. 1) revealed the formation of the polymer as indicated by the absence of alkene-proton signals of 1–3 which should appear between  $\delta$  value of 5.5–6.0 mg·L<sup>-1</sup>.

### 3.2. Corrosion inhibition by TP

The corrosion inhibition ability of TP for St37 corrosion in strong acid environments was assessed using electrochemical approaches. For results obtained from electrochemical experiments to be valid, the essential requirements of linearity, causality, and stability must be met [12]. Fig. 2 shows the variation of OCP of St37 steel with time in (a) 15% HCl and (b) 15% H<sub>2</sub>SO<sub>4</sub> solutions without and with various concentrations of TP at ambient temperature (25 °C). Although there is a slight difference in the length of time taken for a steady state condition to be attained in the various systems, it is obvious that a quasi-steady-state was achieved in all cases within the 3600 s waiting time hence the electrochemical results presented herein should be valid. In the HCl (Fig. 2(a)) and H<sub>2</sub>SO<sub>4</sub> (Fig. 2(b)) solutions devoid of TP, the initial OCP values of the specimen are – 456 mV/Ag/AgCl and – 440 mV/Ag/AgCl respectively. The presence of TP in these media caused noticeable potential shift towards nobler OCP values indicating the appearance of TP adsorbed layer on the steel surface [13,14].

In Fig. 3 is presented the potentiodynamic polarization curves obtained for St37 steel electrode in (a) 15% HCl and (b) 15% H<sub>2</sub>SO<sub>4</sub> solutions devoid of and containing various concentrations of TP at ordinary temperature. The relevant electrochemical polarization parameters namely, corrosion potential ( $E_{\text{corr}}$ ), corrosion current density ( $I_{\text{corr}}$ ), and the anodic and cathodic slopes ( $\beta_a$ ,  $\beta_c$ ) deduced from the graphs are given in Table 1. Also displayed in Table 1 are the polarization resistance ( $R_p$ ) and corrosion rate (CR) obtained from linear polarization graphs (not shown). The extent of corrosion inhibition (IE) by TP from potentiodynamic polarization and linear

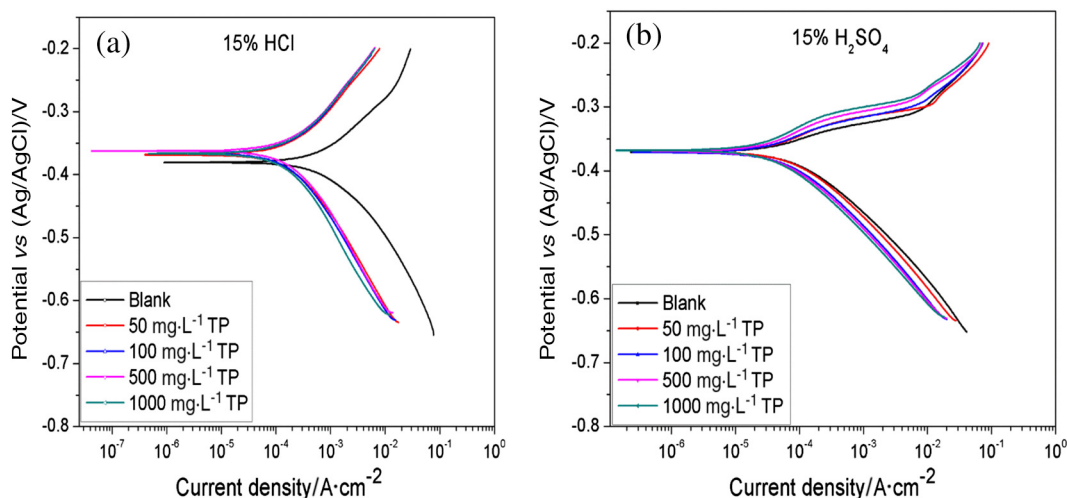


Fig. 3. Potentiodynamic polarization curves for St37 steel in (a) 15% H<sub>2</sub>SO<sub>4</sub> and (b) 15% HCl in the absence and presence of different concentrations TP at 25 °C.

**Table 1**  
Potentiodynamic polarization (PDP) and Linear polarization resistance (LPR) parameters for St37 steel in 15% HCl and 15% H<sub>2</sub>SO<sub>4</sub> without and with different concentrations of TP at 25 °C.

Medium	Concentration/mg·L <sup>-1</sup>	PDP method					LPR method		
		$E_{\text{corr}}$ (Ag/AgCl)/mV	$I_{\text{corr}}$ /μA·cm <sup>-2</sup>	$\beta_a$ /mV·dec <sup>-1</sup>	$\beta_c$ /mV·dec <sup>-1</sup>	IE/%	$R_p$ /Ω·cm <sup>-2</sup>	CR/mpy	IE/%
15% H <sub>2</sub> SO <sub>4</sub>	Blank	-371	63.5	48.6	81.6	-	132.0	120.2	-
	50	-370	56.4	63.4	74.1	11.2	212.0	74.7	37.7
	100	-371	44.0	59.9	74.4	30.7	280.0	56.7	52.9
	500	-370	41.1	70.4	77.5	35.3	318.9	49.8	58.6
	1000	-368	35.2	72.0	79.4	44.6	363.0	43.7	63.6
15% HCl	Blank	-381	649.0	87.6	89.5	-	35.6	445.8	-
	50	-368	211.0	107.6	148.3	67.5	67.5	235.2	47.2
	100	-366	191.0	101.5	131.8	70.6	86.3	183.3	58.8
	500	-362	188.0	104.0	167.4	71.0	120.5	131.7	70.5
	1000	-367	183.0	93.4	130.0	71.8	159.1	99.8	77.6

Note: 1mpy=0.0254mm·a<sup>-1</sup>.

polarization techniques was computed making use of the  $I_{\text{corr}}$  and  $R_p$  values respectively according to the following equations:

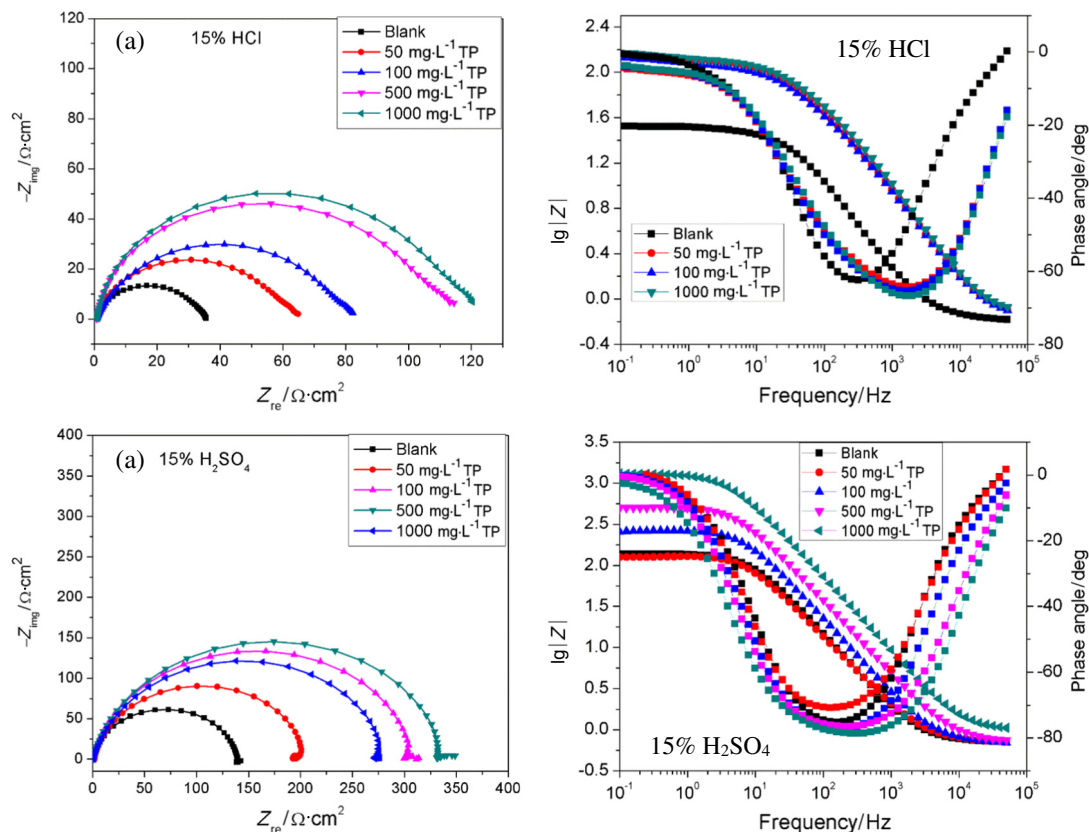
$$IE = \frac{I_{\text{corr(Blank)}} - I_{\text{corr(TP)}}}{I_{\text{corr(Blank)}}} \times 100\% \quad (1)$$

$$IE = \frac{R_{p(\text{TP})} - R_{p(\text{Blank})}}{R_{p(\text{TP})}} \times 100\% \quad (2)$$

From Fig. 3, it is observed that addition of TP to the corrosive media has minimal influence on  $E_{\text{corr}}$ , i.e. the corrosion potential is only shifted slightly towards anodic direction. Both the oxidative dissolution of St37 steel electrode in the anodic region and the hydrogen reduction in the cathodic region are suppressed. These observations are common with mixed type corrosion inhibitors [15,16]. The changes in both  $\beta_a$  and  $\beta_c$  values relative to those of the blank (Table 1) also point to the mixed type behavior of TP in the studied environments [15,16]. A quick

comparison of Fig. 3(a) to (b) reveals that TP is a better corrosion inhibitor for St37 steel in HCl environment than in H<sub>2</sub>SO<sub>4</sub> medium. As could be seen in the figure and in Table 1, there is a remarkable reduction in  $I_{\text{corr}}$  by TP relative to the blank in HCl solution than in H<sub>2</sub>SO<sub>4</sub> solution. For instance, in H<sub>2</sub>SO<sub>4</sub> solution, the addition of 1000 ppm TP resulted in a decline in  $I_{\text{corr}}$  value from 63.5 μA·cm<sup>-2</sup> to 35.2 μA·cm<sup>-2</sup> and the calculated IE is 44.6%. The addition of the same concentration of TP to 15% HCl solution caused a decrease in  $I_{\text{corr}}$  value from 649.0 μA·cm<sup>-2</sup> to 183.0 μA·cm<sup>-2</sup> with 71.8% as the IE. This seems to suggest that the anions (chlorides in HCl and sulphates in H<sub>2</sub>SO<sub>4</sub>) played a vital role in the adsorption process of TP onto the steel surface. It is also observed from the table that the  $I_{\text{corr}}$  and CR values decrease while  $R_p$  and IE values increase with increasing TP concentration. This could mean availability of more inhibitor molecules for adsorption as the concentration increases.

Fig. 4 shows the electrochemical impedance spectroscopy (EIS) results obtained for ST37 steel in free 15% HCl and 15% H<sub>2</sub>SO<sub>4</sub> solutions



**Fig. 4.** EIS plots for St37 steel in 15% H<sub>2</sub>SO<sub>4</sub> and 15% HCl in the absence and presence of different concentrations of TP at 25 °C in (a) Nyquist and (b) Bode representations.

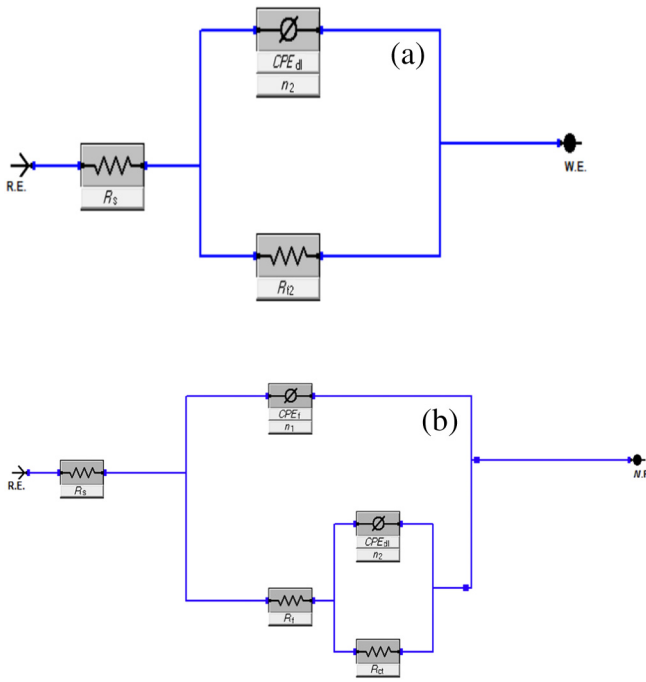


Fig. 5. Equivalent circuit diagrams used to fit impedance data in the (a) blank and (b) presence of TP.

and in the acid solutions fortified with various concentrations of TP in different formats namely (a, c) Nyquist and (b, d) Bode and Phase angle. In the Nyquist diagrams recorded in the free acid solutions, single capacitive loops often linked to charge transfer corrosion process are observed in the high frequencies and they correspond to one time constant in the Bode and Phase angle representations. In the case of TP inhibited systems, two capacitive loops corresponding to two time constants in Fig. 4 (b, d) at the high and medium frequencies can be identified. The two time constants could arise from the double layer structure of the TP adsorbed film on the steel surface [17–19]. To this end, a simple RQR equivalent circuit (Fig. 5(a)) was used for the fitting of the Nyquist curves recorded in the uninhibited systems while the RQ(RQR) equivalent circuit (Fig. 5(b)) was deployed for the analysis of the Nyquist graphs obtained in the TP inhibited acid solutions.

The quite small chi-square values (in the range  $19.4 \times 10^{-5}$  –  $82.4 \times 10^{-5}$ ) (Table 2) and the low values of fitting errors associated with the parameters (less than 5% in all cases) suggested the fitted results were reliable. Accordingly, the physical meanings of the elements in Fig. 5(b) are as follow;  $R_s$  represents the solution resistance,  $R_{f1}$  and  $CPE_f$  stand for the resistance and constant phase element of the outer layer of the adsorbed TP film respectively,  $R_{d1}$  and  $CPE_d$  denote

the resistance and constant phase element of the inner layer of the adsorbed inhibitor film respectively [18,19]. The use of CPE was essential for good quality fit owing to the imperfectness of the capacitive loops [19]. The performance of adsorbed inhibitor film can be judged from the polarization resistance ( $R_p$ ) since inhibition efficiency varies directly with film corrosion resistance [19]. The parameter  $R_p$  is defined as  $R_p = (Z_f \omega = 0)$  [18,19], where  $Z_f$  = faradaic impedance of circuit and  $\omega$  = angular frequency. According to Wang *et al.* [19],  $R_p$  can be expressed as the summation of the resistances of the outer and inner film layers (i.e.  $R_p = R_{f1} + R_{d1}$ ). For the uninhibited system,  $R_p = R_{t2}$ . Therefore, the corrosion protection performance of the TP adsorbed film was evaluated making use of  $R_p$  values according to the following equation:

$$IE = \frac{R_{p(\text{inhibited})} - R_{p(\text{uninhibited})}}{R_{p(\text{inhibited})}} \times 100\% \quad (3)$$

The values of all the parameters associated with the evaluated systems from this technique are displayed in Table 2. From the table, it can be deduced that charge transfer process was difficult in the inhibited systems compared to the uninhibited and this phenomenon may have been caused by the adsorption of TP molecules onto the St37 electrode surface in the inhibited systems. The influence of increase in TP concentration on the  $R_{t2}$  and  $R_p$  of the adsorbed film is obvious in Table 2 and Fig. 4. For instance, the diameter of the Nyquist graphs (Fig. 4(a, c)), impedance and phase angle (Fig. 4(b, d)), the  $R_{t2}$  and  $R_p$  values increased with increasing TP concentration. Increase in inhibitor concentration may have resulted in larger surface coverage. Interestingly, the values of  $R_{f1}$  is found to increase with increase in TP concentration in  $H_2SO_4$  systems but decreases in HCl systems yet the inhibitor performed better in HCl medium than in  $H_2SO_4$  solution. This may reflect the dependency of corrosion protection ability of adsorbed film on the resistive strength of the inner layer than the outer layer. Based on the values of  $n_1$  and  $n_2$  (Table 2) which are near unity, it is concluded that the interface behaved nearly capacitive since  $n = 0$  represents a pure resistor,  $n = -1$  inductor, and  $n = +1$  denotes a pure capacitor [7,11].

To further confirm the corrosion inhibition effect of TP on St37 steel in the considered acid solutions, electrochemical frequency modulation (EFM) was undertaken. The beauty of EFM lies on the inherent data validation control through the use of causality factors (CF-2 and CF-3). As a rule, EFM results are adjudged valid only when the values of CF-2 and CF-3 are within the range 0–2 and 0–3 respectively [4,20]. The representative EFM spectra for ST37 electrodes in the studied media are shown in Fig. 6. Two sets of peaks characterized the spectra – intense and clouded peaks. The intense peaks represent the harmonic and intermodulation signals while the clouded bands represent the background noise signals [4,21]. Only the harmonic and intermodulation peaks were therefore selected for the computation of the corrosion parameters listed in Table 3. The values of  $I_{\text{corr}}$  and CR in the table vary in similar manner as those in Table 1 with TP concentration. Again, both  $\beta_a$

Table 2

Impedance parameters for St37 steel in 15% HCl and 15%  $H_2SO_4$  without and with different concentrations of TP at 25 °C

Medium	Concentration/mg · L <sup>-1</sup>	$R_s/\Omega \cdot \text{cm}^{-2}$	$CPE_f$			$CPE_{dl}$			$R_p/\Omega \cdot \text{cm}^{-2}$	$\chi^2 \times 10^{-5}$	IE/%
			$Y_{01}/\mu\Omega \cdot \text{s}^{n_1} \cdot \text{cm}^{-2}$	$n_1$	$R_{f1}/\Omega \cdot \text{cm}^{-2}$	$Y_{02}/\mu\Omega \cdot \text{s}^{n_2} \cdot \text{cm}^{-2}$	$n_2$	$R_{d1}/\Omega \cdot \text{cm}^{-2}$			
15% $H_2SO_4$	Blank	0.74	–	–	–	141.7	0.93	129.6	129.6	20.9	–
	50	0.65	124.3	0.91	61.3	6240	0.99	138.1	199.4	50.	35.0
	100	0.81	89.7	0.91	79.8	21.2	0.94	196.4	276.2	27.9	53.1
	500	0.76	69.7	0.93	135.2	4016	0.88	169.5	304.7	26.9	57.4
	1000	0.77	68.2	0.92	156.7	560.7	0.87	176.7	333.4	19.4	61.1
15% HCl	Blank	0.65	–	–	–	328.3	0.86	32.1	32.1	56.8	–
	50	0.70	201.7	0.84	4.2	1361.0	0.96	60.3	64.5	43.9	50.2
	100	0.69	242.7	0.80	39.5	1687.0	0.99	40.7	80.2	33.8	59.9
	500	0.79	238.2	0.93	13.2	851.3	0.79	103.7	116.9	66.2	72.5
	1000	0.75	32.8	0.90	4.1	851.3	0.93	152.3	156.4	82.4	79.5

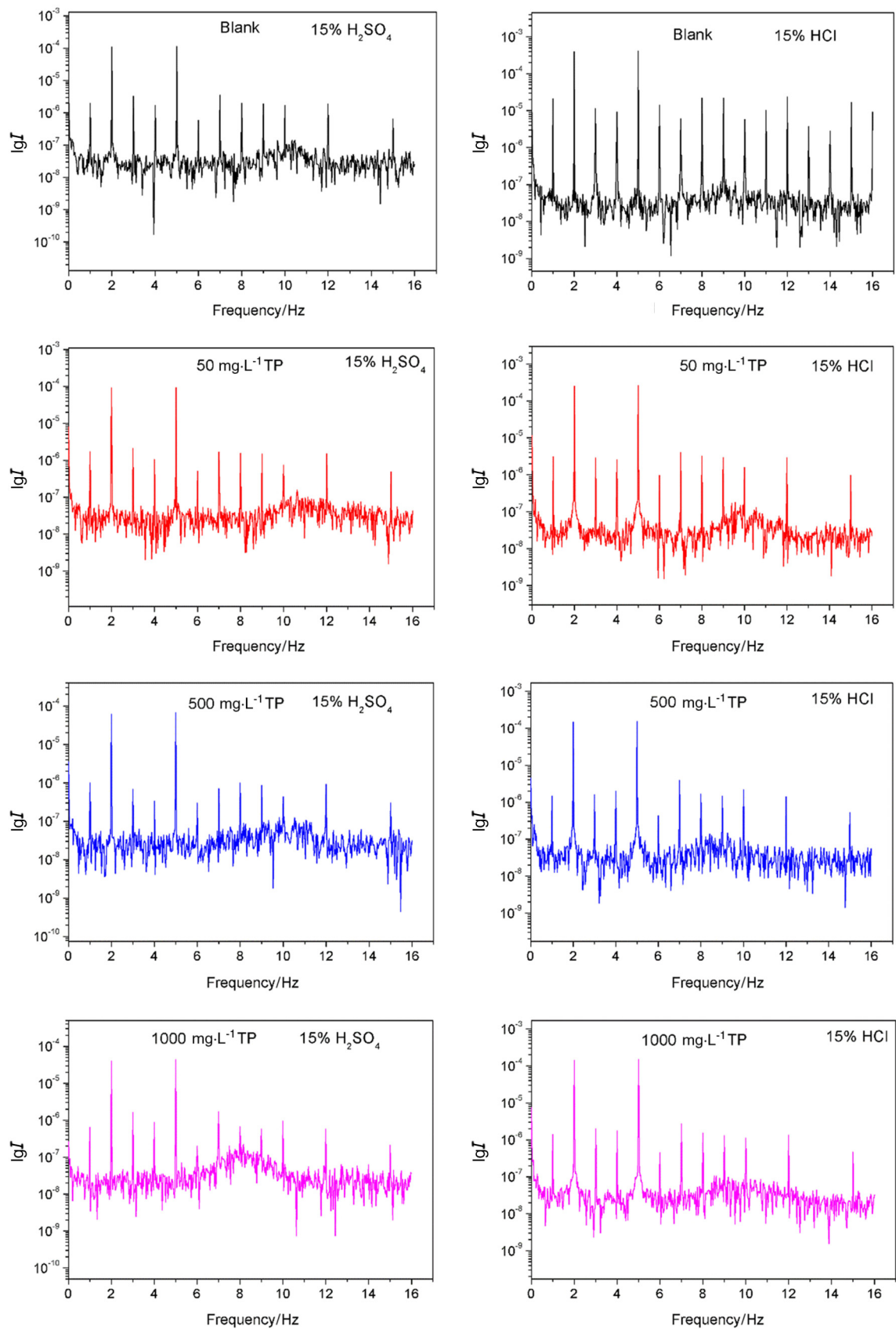


Fig. 6. Intermodulation spectrum recorded for St37 steel in 15% HCl solution in absence and presence of different concentrations of TP at 25 °C.

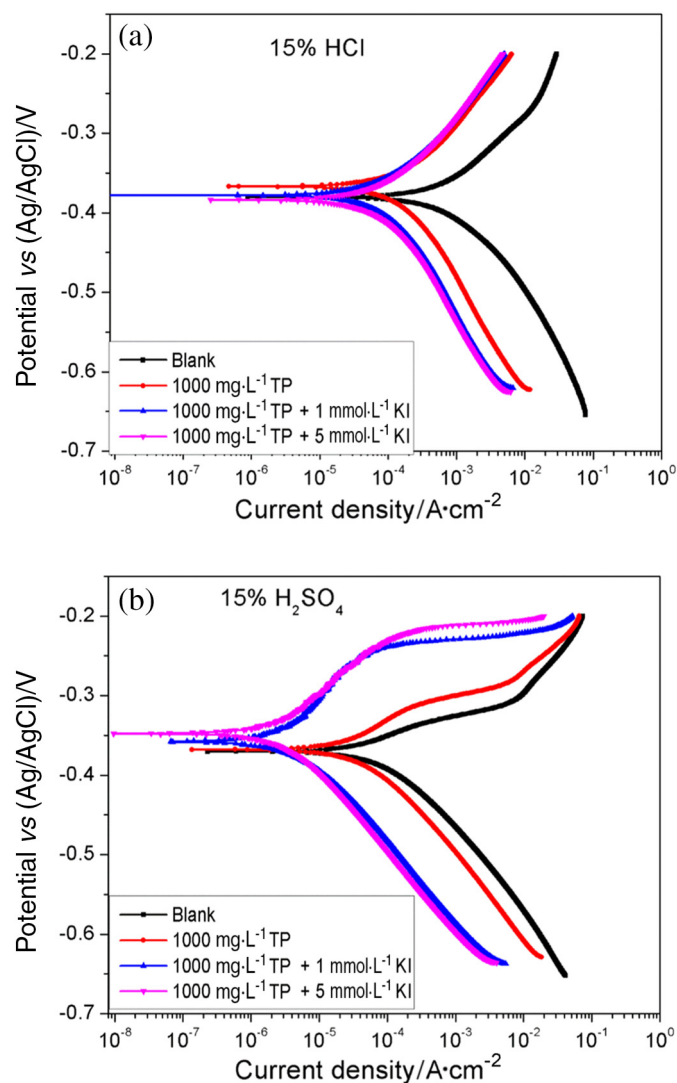
**Table 3**Electrochemical frequency modulation parameters for St37 steel in 15% HCl and 15% H<sub>2</sub>SO<sub>4</sub> in the absence and presence of different concentrations of TP at 25 °C

Medium	Concentration/mg·L <sup>-1</sup>	$I_{corr}/\mu\text{A}\cdot\text{cm}^{-2}$	$\beta_a/\text{mV}\cdot\text{dec}^{-1}$	$\beta_c/\text{mV}\cdot\text{dec}^{-1}$	CR/mpy	CF-2	CF-3	IE/%
15% H <sub>2</sub> SO <sub>4</sub>	Blank	150.1	81.4	96.1	91.4	2.00	3.06	–
	50	112.3	88.2	107.8	68.4	1.92	3.13	25.2
	100	82.5	90.7	105.9	50.2	1.82	3.17	45.0
	500	72.1	87.8	121.1	43.9	1.85	2.86	51.9
	1000	62.7	87.0	110.7	38.2	1.45	2.98	58.2
15% HCl	Blank	928.0	95.9	105.7	533.7	1.69	3.13	–
	50	412.4	101.6	111.4	251.3	1.62	3.13	55.6
	100	334.2	102.3	111.8	203.6	1.54	3.16	63.9
	500	286.8	127.1	138.1	175.9	1.39	3.14	69.1
	1000	264.0	111.5	125.3	160.8	1.64	3.06	71.6

and  $\beta_c$  values are affected with increasing TP concentration supporting the mixed type behavior of TP earlier proposed. The CF-2 and CF-3 values are within the acceptable limits and thus valid the obtained EFM results. There is good agreement between the IE values obtained from this technique with those from other electrochemical techniques (Tables 1 & 2).

### 3.3. Effect of KI on TP performance

In a couple of our previous reports [22–24], we had demonstrated the enhanced corrosion inhibition of polymers by iodide ions due to their strong chemisorption ability. In this present work, it was reasonable to attempt a strategy through which the corrosion inhibition strength of TP can be improved owing to the fact that, the optimum concentration of the polymer (1000 mg·L<sup>-1</sup>) could only afford 55.5% and 63.4% corrosion inhibition to St37 steel in 15% HCl and 15% H<sub>2</sub>SO<sub>4</sub> media respectively. In this regard, we added small amounts (1 mmol·L<sup>-1</sup> and 5 mmol·L<sup>-1</sup>) of KI to the optimum concentration of TP and the effect of this addition on the inhibition efficiency was studied using PDP, LPR, EIS, and EFM. Fig. 7 shows the comparative PDP graphs of St37 steel in (a) 15% HCl and (b) 15% H<sub>2</sub>SO<sub>4</sub> solutions without and containing 1000 mg·L<sup>-1</sup> TP, 1000 mg·L<sup>-1</sup> TP + 1 mmol·L<sup>-1</sup> KI, and 1000 mg·L<sup>-1</sup> TP + 5 mmol·L<sup>-1</sup> KI respectively. All the polarization parameters derived from the graphs are given in Table 4. Obviously, the addition of iodide ions to TP was a beneficial strategy. In Fig. 7 and Table 4, it is very clear that the addition of KI to TP resulted in significant reduction in the corrosion current densities than that of TP alone. This reduction manifested in higher corrosion protection. For instance, on addition of 1 mmol·L<sup>-1</sup> KI and 5 mmol·L<sup>-1</sup> KI to 1000 mg·L<sup>-1</sup> TP, the  $I_{corr}$  values of 35.2  $\mu\text{A}\cdot\text{cm}^{-2}$  and 183.0  $\mu\text{A}\cdot\text{cm}^{-2}$  for TP alone in H<sub>2</sub>SO<sub>4</sub> and HCl solutions respectively were drastically reduced to 4.1  $\mu\text{A}\cdot\text{cm}^{-2}$  and 2.9  $\mu\text{A}\cdot\text{cm}^{-2}$  in H<sub>2</sub>SO<sub>4</sub> medium and 78.3  $\mu\text{A}\cdot\text{cm}^{-2}$  and 76.4  $\mu\text{A}\cdot\text{cm}^{-2}$  in HCl solution. The inhibition efficiency was upgraded from 44.8% in H<sub>2</sub>SO<sub>4</sub> solution to 93.5% and 95.4% on addition of 1 mmol·L<sup>-1</sup> KI and 5 mmol·L<sup>-1</sup> KI respectively. Similarly, the IE of TP in HCl was raised from 71.8% to 87.9% and 88.2% by the addition of 1 mmol·L<sup>-1</sup> KI and 5 mmol·L<sup>-1</sup> KI respectively. This is a clear indication that the TP + KI adsorbed protective film covered greater surface area than TP adsorbed film and probably were more stable. A close inspection of Fig. 7(a) reveals that TP + KI mixture suppressed cathodic reactions more than the anodic reactions. In the anodic branches of the TP + KI graphs in Fig. 7(b), at corrosion potential nobler than -250 mV/(Ag/AgCl), the inhibition effect of the mixture seems to decline and remain near constant for a wide range of potential. For instance, the graphs appear somewhat parallel to the x-axis. Qian *et al.* [25] had reported similar observation and was interpreted to mean desorption potential where the desorption rate of the adsorbed film is higher than the adsorption rate. By comparing the IE values of TP + KI in HCl systems to those in H<sub>2</sub>SO<sub>4</sub> solutions (Table 4), it is found that the values are higher in H<sub>2</sub>SO<sub>4</sub> than HCl which is a reverse of what was observed in the case of TP alone (Tables 1–3). The possible cause of this reversal is explained in Section 3.6. In Table 4 is also presented the  $R_p$ , CR, and IE values obtained from LPR measurements for the studied substrate and systems. In both acid media, the polarization and corrosion rate of the substrate are greatly reduced by TP + KI mixture but the effect is more in H<sub>2</sub>SO<sub>4</sub> medium than HCl and thus agree with the PDP findings. IE of 94.9% and 95.8% are obtained from this technique for TP + 1 mmol·L<sup>-1</sup> KI



**Fig. 7.** Potentiodynamic polarization curves for St37 steel in (a) 15% H<sub>2</sub>SO<sub>4</sub> and (b) 15% HCl in the absence and presence of TP (1000 mg·L<sup>-1</sup>) and TP + KI mixtures at 25 °C.

**Table 4**  
Potentiodynamic polarization (PDP) and Linear polarization resistance (LPR) parameters for St37 steel in 15% HCl and 15% H<sub>2</sub>SO<sub>4</sub> without, with 1000 mg/L TP, KI and TP + KI mixtures at 25 °C.

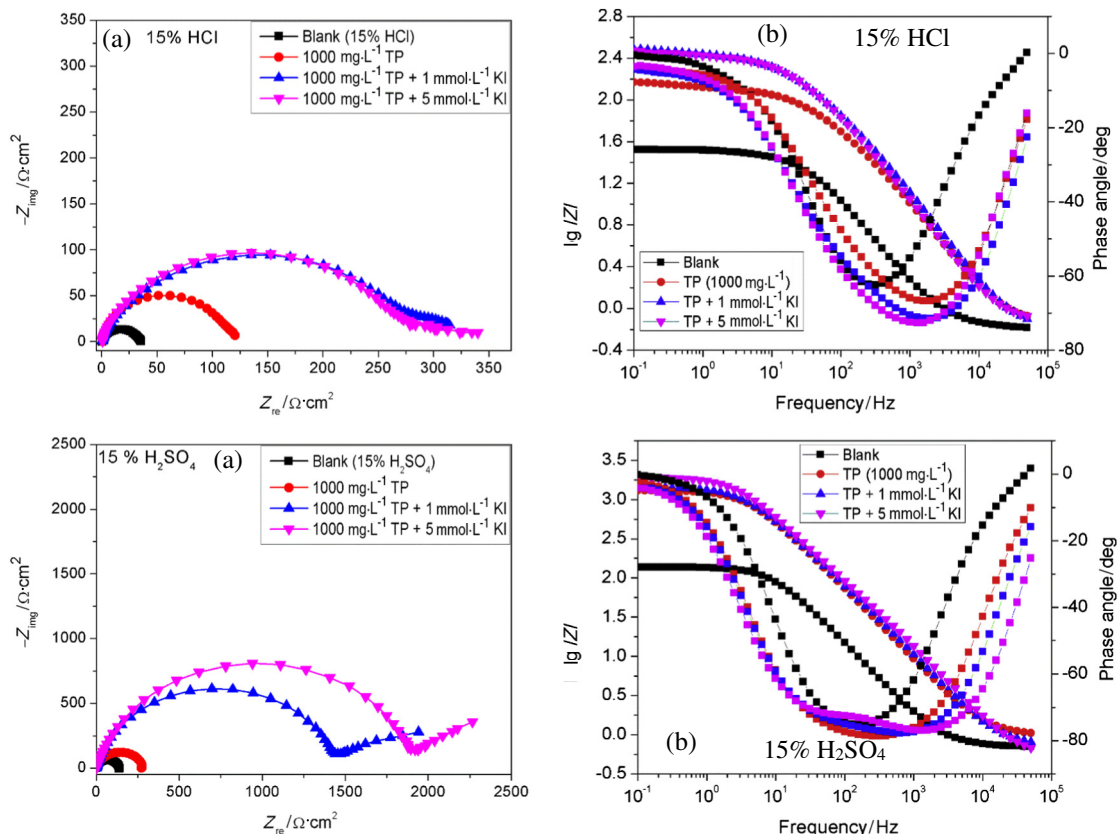
Medium	Concentration	PDP method					LPR method		
		$E_{corr}$ (Ag/AgCl)/mV	$I_{corr}/\mu\text{A}\cdot\text{cm}^{-2}$	$\beta_a/\text{mV}\cdot\text{dec}^{-1}$	$\beta_c/\text{mV}\cdot\text{dec}^{-1}$	$IE/\%$	$R_p/\Omega\cdot\text{cm}^2$	$CR/\text{mpy}$	$IE/\%$
15% H <sub>2</sub> SO <sub>4</sub>	Blank	-371	63.5	48.6	81.6	–	132.0	120.2	–
	TP (1000 mg·L <sup>-1</sup> )	-368	35.2	72.0	79.4	44.8	363.0	43.7	63.4
	1 mmol·L <sup>-1</sup> KI	-363	4.3	120.6	85.4	93.2	1811	8.8	92.7
	5 mmol·L <sup>-1</sup> KI	-347	3.8	127.1	115.4	94.0	2143	7.4	93.8
	TP + 1 mmol·L <sup>-1</sup> KI	-358	4.1	126.4	79.7	93.5	2593	6.1	94.9
	TP + 5 mmol·L <sup>-1</sup> KI	-348	2.9	82.3	96.9	95.4	3158	5.0	95.8
15% HCl	Blank	-381	649.0	87.6	89.5	–	35.6	445.8	–
	TP (1000 mg·L <sup>-1</sup> )	-367	183.0	104.0	167.4	71.8	159.1	99.8	77.6
	1 mmol·L <sup>-1</sup> KI	-386	218.0	77.6	91.2	66.4	80.0	198.4	55.5
	5 mmol·L <sup>-1</sup> KI	-397	158.0	80.4	108.7	75.7	116.2	136.6	69.4
	TP + 1 mmol·L <sup>-1</sup> KI	-378	78.3	82.0	120.0	87.9	313.8	50.58	88.7
	TP + 5 mmol·L <sup>-1</sup> KI	-384	76.4	84.7	125.1	88.2	331.8	47.8	89.3

and TP + 5 mmol·L<sup>-1</sup> KI respectively in H<sub>2</sub>SO<sub>4</sub> solution while the values are 88.7% and 89.3% in HCl environment.

The Nyquist, Bode, and Phase angle plots for St37 steel in (a, b) 15% HCl and (c, d) 15% H<sub>2</sub>SO<sub>4</sub> solutions without and with additives are shown in Fig. 8. The equivalent circuit in Fig. 5(b) was used for the analysis of the TP + KI Nyquist graphs. All the parameters pertaining to these systems are given in Table 5. As could be seen in Fig. 8(a, c), the semicircles at high frequencies in the TP + KI Nyquist graphs are outstandingly larger than those of TP alone and the second loop in the medium frequencies becomes very pronounced. There is also a noticeable displacement in the impedance and phase angle in Fig. 8(b, d) on the addition of KI to TP. All these indicate the enhancement in corrosion inhibition efficiency of TP by KI. The results in Table 5 reveals that the polarization resistance of St37 steel in the acid solutions was increased by a factor of more than 10 on the introduction of KI into the corrosive systems containing 1000 mg·L<sup>-1</sup> TP. It can be concluded from the

results in Table 5 that in 15% H<sub>2</sub>SO<sub>4</sub> environment, ST37 steel surface can be protected against corrosion by 93.4% and 93.5% while in 15% HCl, corrosion protection of 79.5% and 89.7% can be achieved on the addition of 1 mM KI and 5 mM KI respectively to 1000 mg·L<sup>-1</sup> TP.

Fig. 9 shows the EFM spectra recorded for St37 steel in strong acid media without and with various additives as corrosion inhibitor and the parameters deduced from the analysis of the spectra are presented in Table 6. The obtained CF-2 and CF-3 values are within the acceptable limit and the  $I_{corr}$  values are in perfect agreement with those derived from PDP experiments. There is also clear evidence of improved TP corrosion inhibition efficiency by KI addition. The IE values from all the electrochemical techniques are in good agreement and point to synergistic corrosion inhibition between TP and iodide ions. To determine whether the observed improvement in the corrosion inhibition efficiency of TP upon combination with iodide ions is due to synergistic effect, we calculated the synergism parameter ( $S_1$ ). As it is known,

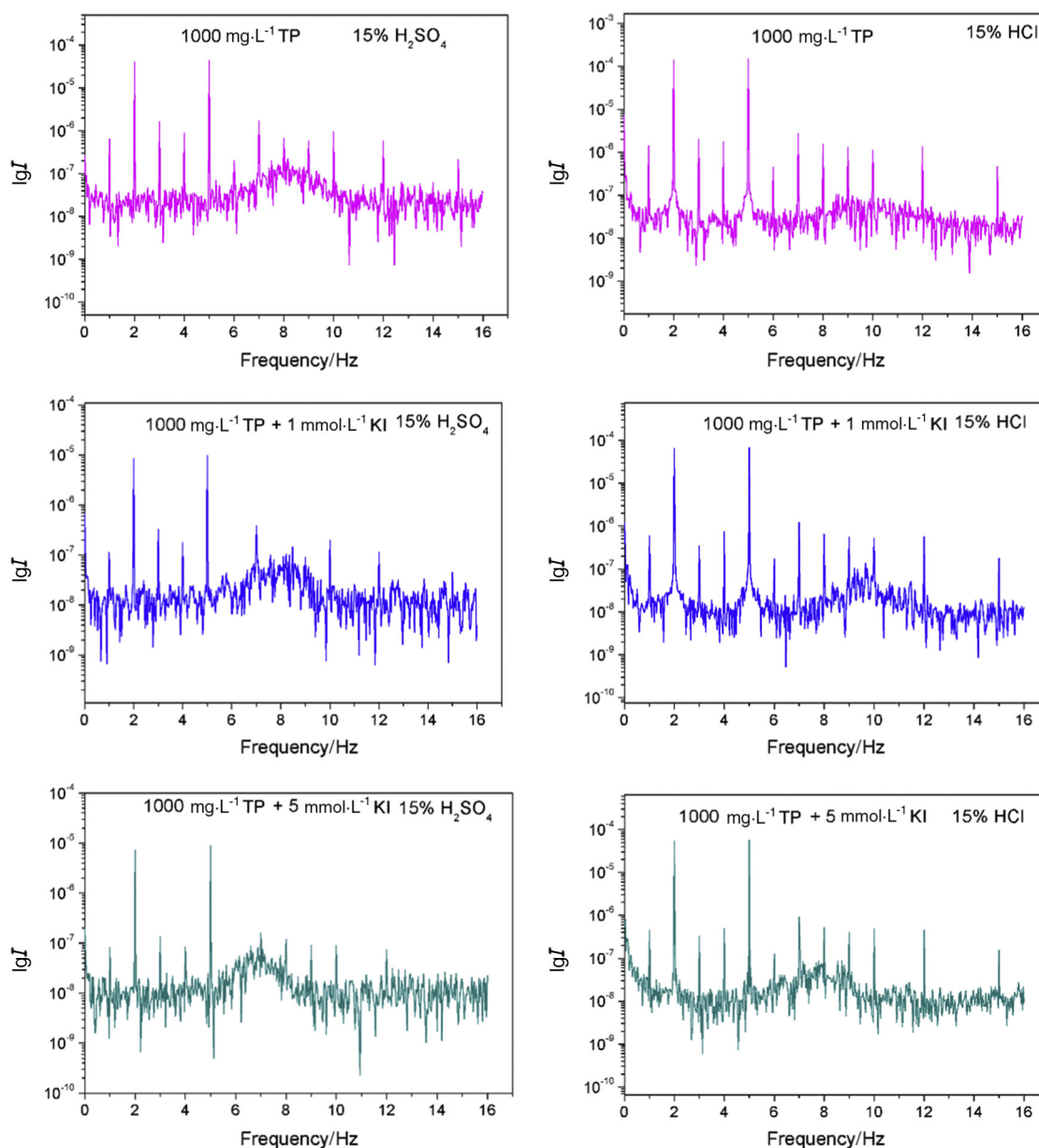


**Fig. 8.** EIS plots for St37 steel in 15% H<sub>2</sub>SO<sub>4</sub> and 15% HCl in the absence and presence of TP (1000 mg·L<sup>-1</sup>) and TP + KI mixtures at 25 °C in (a) Nyquist and (b) Bode representations.



**Table 5**Impedance parameters for St37 steel in 15% HCl and 15% H<sub>2</sub>SO<sub>4</sub> without, with 1000 mg·L<sup>-1</sup> TP and TP + KI mixtures at 25 °C

Medium	Concentration	CPE <sub>f</sub>			CPE <sub>d1</sub>			R <sub>ct</sub> /Ω·cm <sup>-2</sup>	R <sub>p</sub> /Ω·cm <sup>-2</sup>	χ <sup>2</sup> × 10 <sup>-5</sup>	IE/%
		R <sub>e</sub> /Ω·cm <sup>-2</sup>	Y <sub>o1</sub> /μΩ·s <sup>n1</sup> ·cm <sup>-2</sup>	n <sub>1</sub>	R <sub>f</sub> /Ω·cm <sup>-2</sup>	Y <sub>o2</sub> /μΩ·s <sup>n2</sup> ·cm <sup>-2</sup>	n <sub>2</sub>				
15% H <sub>2</sub> SO <sub>4</sub>	Blank	0.74	–	–	–	141.7	0.93	129.6	129.6	20.9	–
	TP (1000 mg·L <sup>-1</sup> )	0.77	68.2	0.92	156.7	40.9	0.87	176.7	333.4	19.4	61.1
	1 mmol·L <sup>-1</sup> KI	0.74	71.4	0.89	263.2	54.2	0.99	1052.0	1315.2	86.3	90.1
	5 mmol·L <sup>-1</sup> KI	0.76	67.4	0.88	302.9	52,450	0.99	1362.0	1664.9	124.9	92.2
	TP + 1 mmol·L <sup>-1</sup> KI	0.71	39.8	0.90	506.5	17,060	0.96	1456.0	1962.5	146.6	93.4
15% HCl	TP + 5 mmol·L <sup>-1</sup> KI	0.60	15.9	0.96	81.2	29.9	0.78	1923.0	2004.2	204.6	93.5
	Blank	0.65	–	–	–	328.3	0.86	32.1	32.1	56.8	–
	TP (1000 mg·L <sup>-1</sup> )	0.75	32.8	0.90	4.1	851.3	0.39	152.3	156.4	82.4	79.5
	1 mmol·L <sup>-1</sup> KI	0.76	86.9	0.92	11.6	219.4	0.62	64.0	75.6	15.8	57.6
	5 mmol·L <sup>-1</sup> KI	0.80	49.2	0.94	13.0	94.7	0.72	100.1	113.1	18.0	71.7
	TP + 1 mmol·L <sup>-1</sup> KI	0.72	13.2	0.97	13.2	211.7	0.56	298.3	311.5	66.3	89.7
	TP + 5 mmol·L <sup>-1</sup> KI	0.74	36.2	0.90	0.00	448.4	0.26	339.9	339.9	119.0	90.6

**Fig. 9.** Intermodulation spectrum recorded for St37 steel in 15% HCl solution in the absence and presence of TP (1000 mg·L<sup>-1</sup>) and TP + KI mixtures at 25 °C.

**Table 6**  
Electrochemical frequency modulation parameters for St37 steel in 15% HCl and 15% H<sub>2</sub>SO<sub>4</sub> in the absence, presence of 1000 mg·L<sup>-1</sup> TP, KI and TP + KI mixtures at 25 °C

Medium	Concentration	$I_{corr}/\mu\text{A}\cdot\text{cm}^{-2}$	$\beta_a/\text{mV}\cdot\text{dec}^{-1}$	$\beta_c/\text{mV}\cdot\text{dec}^{-1}$	CR/mpy	CF-2	CF-3	IE/%
15% H <sub>2</sub> SO <sub>4</sub>	Blank	150.1	81.4	96.1	91.4	2.00	3.06	–
	TP (1000 mg·L <sup>-1</sup> )	62.7	87.0	110.7	38.2	1.45	2.98	58.2
	1 mmol·L <sup>-1</sup> KI	18.4	89.5	112.8	11.2	2.44	2.74	87.7
	5 mmol·L <sup>-1</sup> KI	15.4	89.61	100.2	9.4	2.08	2.65	89.7
	TP + 1 mmol·L <sup>-1</sup> KI	16.5	103.6	137.8	10.1	1.89	3.50	89.0
	TP + 5 mmol·L <sup>-1</sup> KI	13.6	102.9	116.2	8.3	1.68	2.79	90.9
	Blank	928.0	95.9	105.7	533.7	1.69	3.13	–
15% HCl	TP (1000 mg·L <sup>-1</sup> )	264.0	111.5	125.3	160.8	1.64	3.06	71.6
	1 mmol·L <sup>-1</sup> KI	317.3	95.7	102.8	193.3	1.91	3.12	65.8
	5 mmol·L <sup>-1</sup> KI	188.7	88.2	98.2	115.0	1.93	3.09	79.7
	TP + 1 mmol·L <sup>-1</sup> KI	125.1	117.6	128.7	76.2	1.27	3.31	86.5
	TP + 5 mmol·L <sup>-1</sup> KI	106.6	127.7	132.0	64.9	1.30	3.23	88.5

**Table 7**  
Calculated values of the synergism parameter ( $S_1$ ) from the various methods used

Inhibitor mixture	PDP	LPR	EIS	EFM
<i>H<sub>2</sub>SO<sub>4</sub></i>				
TP + 1 mmol·L <sup>-1</sup> KI	1.48	1.65	1.63	1.65
TP + 5 mmol·L <sup>-1</sup> KI	1.46	1.65	1.65	1.63
<i>HCl</i>				
TP + 1 mmol·L <sup>-1</sup> KI	1.58	1.51	1.53	1.60
TP + 5 mmol·L <sup>-1</sup> KI	1.68	1.65	1.68	1.72

**Table 8**  
Langmuir adsorption parameters for St37 steel in 15% HCl and 15% H<sub>2</sub>SO<sub>4</sub> containing TP from different experimental methods at 25 °C

Corrosive medium	Experimental methods	$\Delta G_{ads}^0/\text{kJ}\cdot\text{mol}^{-1}$	$K_{ads} \times 10^2/\text{L}\cdot\text{g}^{-1}$	Slope	$R^2$
15% H <sub>2</sub> SO <sub>4</sub>	LPR	-24.30	1.82	1.52	0.998
	EIS	-24.37	1.87	1.59	0.996
	EFM	-22.82	1.00	1.64	0.998
15% HCl	LPR	-24.39	1.89	1.24	0.998
	EIS	-24.54	2.00	1.21	0.999
	EFM	-26.36	4.18	1.37	0.998

iodide ions and organic inhibitors can co-adsorb on a metal surface in two ways; competitive or cooperative [26,27]. In competitive co-adsorption, iodide ions and organic cations adsorb on different sites in the metal surface [26] whereas in cooperative co-adsorption, the iodide ions first chemisorb on the metal surface and the organic cations adsorb

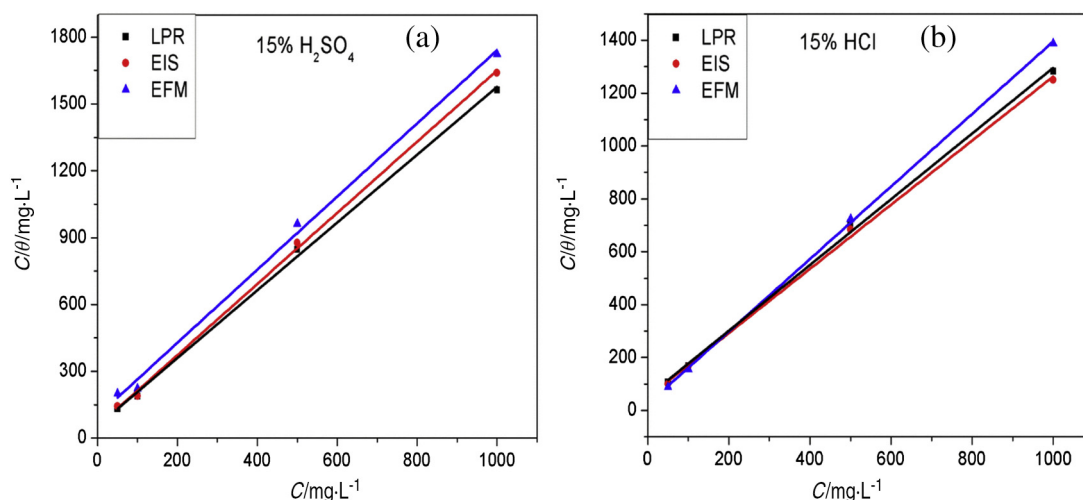
on iodide ions adsorbed layer [26]. Competitive co-adsorption leads to antagonistic effect while cooperative co-adsorption gives rise to synergistic effect [26,28]. These two forms of co-adsorption can be differentiated using the synergism parameter. A value of  $S_1 < 1$  signifies antagonistic effect while  $S_1 > 1$  points to synergistic effect [26–28]. The synergism parameter can be calculated using the following equation [26,29]:

$$S_1 = \frac{1 - (IE_1 + IE_2)}{1 - IE_{1+2}} \quad (4)$$

where  $IE_1$  is the inhibition efficiency of iodide ions,  $IE_2$  is the inhibition efficiency of the inhibitor,  $IE_{1+2}$  is the inhibition efficiency of inhibitor + iodide ions. In our case, the calculated  $S_1$  values (Table 7) are all greater than unity hence we conclude that the observed improvement on the corrosion inhibition efficiency of TP by iodide ions is due to synergistic effect.

### 3.4. Adsorption isotherm consideration

The use of adsorption isotherm to probe the adsorption characteristics of organic inhibitors is still a valid model [30–32]. The adsorption of organic inhibitor on metal surface depends on the degree of surface coverage ( $\theta$ ) [30]. The degree of surface coverage ( $\theta$ ) at different concentrations of TP on the St37 steel surface was calculated from the  $IE$  values ( $\theta = IE/100$ ) obtained from LPR, EIS, and EFM experiments (Tables 1–3). By virtue of the linear regression coefficient ( $R^2$ ) value which was approximately 1 in all cases (Table 8), the Langmuir



**Fig. 10.** Langmuir adsorption isotherm for St37 steel in (a) 15% H<sub>2</sub>SO<sub>4</sub> and (b) 15% HCl containing TP from different experimental techniques.

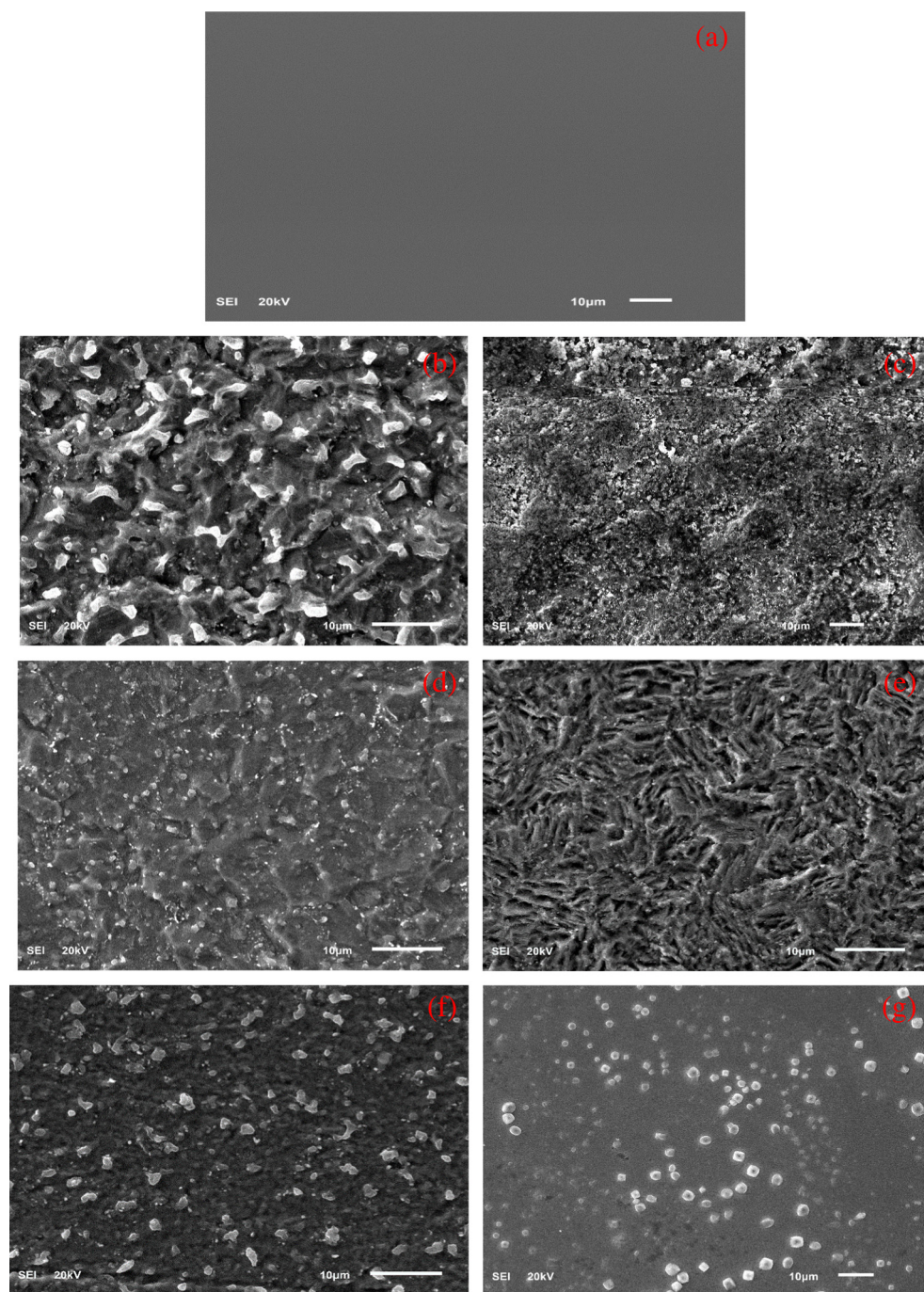
adsorption isotherm was selected as the best fit isotherm for the studied systems. It has the general form:

$$\frac{C_{\text{inh}}}{\theta} = \frac{1}{K_{\text{ads}}} + C_{\text{inh}} \quad (5)$$

where  $C_{\text{inh}}$  is the inhibitor concentration and  $K_{\text{ads}}$  is the equilibrium constant for adsorption–desorption process [14]. The linear relationship for TP adsorption onto St37 steel surface obtained by plotting  $C_{\text{inh}}/\theta$  versus  $C_{\text{inh}}$  is shown in Fig. 10.

As should be expected, the slopes of the graphs (Table 8) slightly deviated from unity required by an ideal Langmuir model indicating the

existence of interaction in the adsorbed layer. Langmuir adsorption equation had been derived on the assumption that adsorbed molecules do not interact with each other [7]. This is not true as authors [7,23,33] have demonstrated that macromolecules like TP in adsorbed layer are capable of interaction. The  $K_{\text{ads}}$  value was computed from the intercepts of the graphs in Fig. 10 and as could be seen in Table 8, the value is low (*i.e.* between  $(1.00\text{--}4.18) \times 10^{-2} \text{ L}\cdot\text{g}^{-1}$ ) demonstrating low proportion of TP adsorbed on the St37 steel surface [14,34,35]. It also suggests less adherence of the TP adsorbed films on the metal surface. The higher the  $K_{\text{ads}}$  value, the tighter the adsorbed inhibitor film on the metal surface and the better the inhibitive ability [31]. To obtain information on the spontaneity of the adsorption process, the adsorption free energy



**Fig. 11.** SEM micrographs for St37 steel (a) in the polished state (b) exposed to 15% HCl, (c) exposed to 15% H<sub>2</sub>SO<sub>4</sub>, (d) exposed to 15% HCl containing 1000 mg·L<sup>-1</sup> TP, (e) exposed to 15% H<sub>2</sub>SO<sub>4</sub> containing 1000 mg·L<sup>-1</sup> TP, (f) exposed to 15% HCl containing 1000 mg·L<sup>-1</sup> TP + 5 mmol·L<sup>-1</sup> KI and (g) exposed to 15% H<sub>2</sub>SO<sub>4</sub> containing 1000 mg·L<sup>-1</sup> TP + 5 mmol·L<sup>-1</sup> KI after 24 h.

( $\Delta G_{\text{ads}}^0$ ) was computed making use of the  $K_{\text{ads}}$  value according to the following equation [31,36]:

$$K_{\text{ads}} = \frac{1}{C_{\text{water}}} \exp\left(\frac{-\Delta G_{\text{ads}}^0}{RT}\right) \quad (6)$$

where  $C_{\text{water}}$  is the water concentration in the solution = 1000 g·L<sup>-1</sup>,  $R$  is the molar gas constant, and  $T$  is the absolute temperature. The calculated  $\Delta G_{\text{ads}}^0$  value from the various experimental methods are also given in Table 8. The value is negative and is indicative of spontaneous adsorption of TP molecules and stability on the St37 steel surface in the studied corrosive media [13,37].

### 3.5. Surface analysis

Fig. 11 shows the surface morphologies of St37 steel samples (a) before and after immersion in (b) 15% HCl solution, (c) 15% H<sub>2</sub>SO<sub>4</sub> solution, (d) 15% HCl + 1000 mg·L<sup>-1</sup> TP, (e) 15% H<sub>2</sub>SO<sub>4</sub> + 1000 mg·L<sup>-1</sup> TP, (f) 15% HCl + 1000 mg·L<sup>-1</sup> TP + 5 mmol·L<sup>-1</sup> KI, and (g) 15% H<sub>2</sub>SO<sub>4</sub> + 1000 mg·L<sup>-1</sup> TP + 5 mmol·L<sup>-1</sup> KI solution for 24 h at 25 °C. Apparently, the smooth morphology of the specimens (Fig. 11(a)) is completely lost to corrosion upon exposure to the acid solutions. The surfaces thereafter exhibit rough and hilly-shaped morphologies (Fig. 11(b & c)). Compared with the surface in Fig. 11(c), the one in Fig. 11(b) is rougher inferring that St37 steel sample deteriorated in 15% HCl solution than in 15% H<sub>2</sub>SO<sub>4</sub> solution. Undoubtedly, the metal samples were protected against corrosion in the acid solutions containing TP as evidenced in the relatively smoother surfaces in Fig. 11(d & e) compared to the ones in Fig. 11(b & c). It was deduced from experimental results (Tables 1–3) that TP retarded St37 steel dissolution in HCl medium than in H<sub>2</sub>SO<sub>4</sub> environment. With a smoother surface morphology as observed in Fig. 11(d) than in Fig. 11(e), the surface analysis results agree with the experimental results. Again, it is obvious that addition of KI to TP enhanced the corrosion inhibition efficiency of TP in the acid environments and the effect is higher in H<sub>2</sub>SO<sub>4</sub> environment than in HCl medium. Clearly, the image in Fig. 11(g) presents smoother morphology than the one in Fig. 11(f) but the surfaces in Fig. 11(d & e) are rougher than the surfaces in Fig. 11(f & g). Based on the experimental and surface analysis results, it is concluded that TP + KI combination offers a good corrosion protection to St37 steel in strong acid environments.

### 3.6. Mechanism of corrosion inhibition

Inhibitors in acid solution can interact with metals and affect the corrosion reaction in a number of ways, some of which may occur simultaneously. It is practically impossible to assign a single general mechanism of action to an inhibitor because the mechanism may change with experimental conditions. Thus, the predominant mechanism of action of an inhibitor may vary with factors such as its concentration, the pH of the acid, the nature of the anion of the acid, the presence of other species in the solution, the extent of reaction to form secondary inhibitors, and the nature of the metal [30,38,39]. Our experimental results reveal that TP inhibits St37 steel corrosion better in HCl solution than H<sub>2</sub>SO<sub>4</sub> solution but TP + KI mixture is a better inhibitor in H<sub>2</sub>SO<sub>4</sub> than HCl solution. Generally, metal corrosion inhibition by adsorption mechanism is a quasi-substitution process and could be by physisorption or chemisorption [40,41]. TP in the strong acids could be protonated and there is every tendency that St37 steel surface acquires net positive charge. Adsorption of protonated forms of TP onto charged St37 steel surface would be greatly influenced by the anions present in the solution. As it is known, in HCl solution, chloride ions are specifically adsorbed on metal surface while sulphate ions are adsorbed in H<sub>2</sub>SO<sub>4</sub> medium [26,28]. The chloride ions have a higher shielding power than the sulphate ions therefore more of protonated TP should be expected to

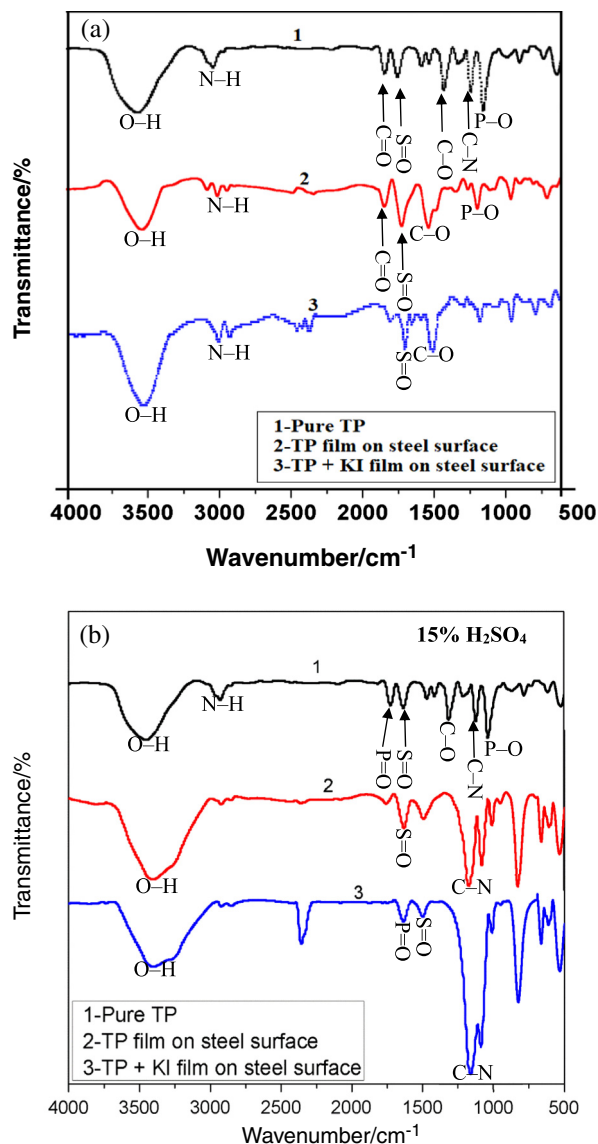


Fig. 12. FTIR spectra of pure TP, and film extracted from St37 surface immersed in (a) 15% HCl and (b) 15% H<sub>2</sub>SO<sub>4</sub> containing TP and TP + KI mixtures.

adsorbed on the St37 steel surface recharged by chloride ions than one recharged by sulphate ions. Nevertheless, adsorbed protonated molecules could be deprotonated and the freed heteroatoms go into coordinate type of bond with metal surface [12,42]. Such complex formation would lead to better corrosion protection [12,42]. To gain insight into the corrosion inhibition of St37 steel in HCl and H<sub>2</sub>SO<sub>4</sub> media by TP and TP + KI and to explain why TP + KI better inhibits in H<sub>2</sub>SO<sub>4</sub> solution than HCl, FTIR and UV-vis experiments were undertaken. Fig. 12 shows the FTIR spectra of pure TP, TP film, and TP + KI film extracted from St37 steel surface after immersion in (a) HCl solution and (b) H<sub>2</sub>SO<sub>4</sub> medium. The spectrum of the pure TP is characterized with peaks at 3500 cm<sup>-1</sup>, 3100 cm<sup>-1</sup>, 1850 cm<sup>-1</sup>, 1613.2 cm<sup>-1</sup>, 1320 cm<sup>-1</sup>, 1282 cm<sup>-1</sup>, and 1000 cm<sup>-1</sup>. They correspond to O—H [7,11], N—H [43], C=O [15], S=O [44], C—O [45], C—N [46], and P—O [45] stretching vibrations respectively. Compared with the TP and TP + KI film spectra in Fig. 12(a), the P—O and S=O peaks shifted to 1100 cm<sup>-1</sup> and 1702 cm<sup>-1</sup> respectively and are more intense, the C—O, C=O, and N—H peaks diminish and are less intense. In Fig. 12(b), the N—H peak almost completely disappears while the C—O peak becomes more intense in the TP and TP + KI spectra compared to the pure TP. All these reflect the involvement of the

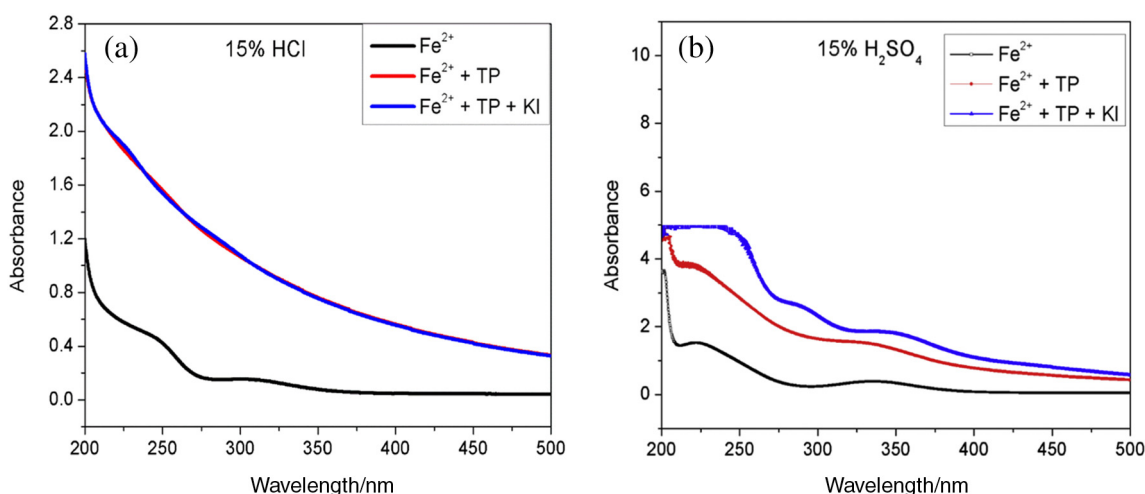


Fig. 13. UV-Vis spectra of (a) 15% HCl and (b) 15% H<sub>2</sub>SO<sub>4</sub> solutions without and with 1000 mg·L<sup>-1</sup> TP and 1000 mg·L<sup>-1</sup> TP + KI mixtures after St37 steel immersion for 24 h at 25 °C.

heteroatoms in the adsorption process. However, the adsorption mechanism seems to be different for TP and TP + KI in HCl and H<sub>2</sub>SO<sub>4</sub> solutions. For instance, the N—H peak is almost absent in the TP and TP + KI spectra in Fig. 12(b) but not so in Fig. 12(a). Also, the C—O peak is stronger in the TP and TP + KI spectra in Fig. 12(b) than in Fig. 12(a) and new peak emerged in the TP + KI spectrum at 2500 cm<sup>-1</sup> in Fig. 12(b). The UV-vis spectra presented in Fig. 13 give a clearer picture to the adsorption processes in the studied systems. The solutions resulting from St37 steel immersion in the acid solutions yielded spectra with two bands, one at 250 nm and the other at 300 nm, while the spectra for 15% HCl containing the additives shows no band. This means that, in the presence of both TP and TP + KI, there was no complex formation. The adsorbed inhibitor films were held on the metal surface by electrostatic force. The non-formation or formation of unstable Fe-inhibitor complex even in the presence of iodide ions in the HCl solution may have been caused by competitive adsorption between Cl<sup>-</sup> and I<sup>-</sup> ions. As it is known, in HCl environment, the specific adsorption of chloride ions is on the anodic site while hydronium ions are adsorbed at the cathodic site [39,47,48]. Our PDP results (Fig. 7(a)) clearly shows that in HCl solution, addition of KI did not affect the anodic reactions but affected only the cathodic reactions. It means that there was some sort of opposition from chloride ions to iodide ions on the anodic site and this may have resulted in formation of unstable or non-formation of complex at all. In the Fe<sup>2+</sup> + TP + KI spectrum of Fig. 13(b), three clear bands at 250 nm, 300 nm, and 350 nm can be identified. The appearance of the new peak at 350 nm justify the formation of Fe-inhibitor complex. Similar submission can be found in the corrosion literature [15]. This new band corresponds to the extra peak at 2500 cm<sup>-1</sup> in Fig. 12(b). The complex so formed in H<sub>2</sub>SO<sub>4</sub> solution ensured better corrosion mitigation than in HCl solution. It should also be mentioned that iodide ions suffered less opposition in H<sub>2</sub>SO<sub>4</sub> solution as evidenced in the PDP result in Fig. 7(b); both the anodic and cathodic reactions are affected by KI addition.

#### 4. Conclusions

A novel tetrapolymer (TP) consisting of carboxylate, sulphonate, phosphonate and sulfur dioxide based co-monomers has been successfully synthesized using Butler cyclopolymerization technique and characterized using FTIR, <sup>1</sup>H-NMR, <sup>13</sup>C NMR and elemental analysis. The tetrapolymer is a moderate corrosion inhibitor for St37 steel in 15% HCl and 15% H<sub>2</sub>SO<sub>4</sub> acid media but better in HCl medium than in H<sub>2</sub>SO<sub>4</sub> solution. Addition of small amount of KI to the tetrapolymer synergistically enhanced TP corrosion inhibition efficiency. 5 mmol·L<sup>-1</sup> KI

upgraded TP corrosion inhibition efficiency from 61.1% and 79.5% in H<sub>2</sub>SO<sub>4</sub> and HCl solutions respectively to 93.5% and 90.6% according to the EIS results. TP and TP + KI afforded the corrosion inhibition of St37 steel in the acid media by virtue of adsorption mechanism according to ATR-FTIR analysis results and the adsorption process followed Langmuir adsorption isotherm. TP + KI formed complex with St37 steel surface in H<sub>2</sub>SO<sub>4</sub> solution but not in HCl solution.

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