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Study of the development of three-dimensional sets of fluid particles and iso-concentration fields using kinematic simulation

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We use kinematic simulation (KS) to study the development of a material line immersed in a three-dimensional turbulent flow. We generalize this study to a material surface, cube and sphere. We find that the fractal dimension of the surface can be explained by the same mechanism as that proposed by Villermaux & Gagne (Phys. Rev. Lett. vol. 73, 1994, p. 252) for the line. The fractal dimension of the line or the surface is a linear function of time up to times of the order of the smallest characteristic time of turbulence (or Kolmogorov timescale). For volume objects we describe the respective role of the Reynolds number and of the object's characteristic size. Using the method of characteristics with KS we compute the evolution with time of a concentration field C(x, t) and measure the fractal dimension of the intersection of this scalar field with a given plane. For these objects, we retrieve the result of Villermaux & Innocenti (J. Fluid Mech. vol. 393, 1999, p. 123) that the Reynolds number does not affect the development of the fractal dimension of the iso-scalar surface and extend this result to volume geometries. We also find that for volume objects the characteristic time of development of the fractal dimension is the large scales' characteristic time and not the Kolmogorov timescale.

1. Introduction

Mixing is an important and complex problem of fluid mechanics with many practical applications. One way to look at it is to study interface geometry by measuring fractal dimensions. This has led to the definition of burning rates using the flamelet approach (see e.g. Gouldin 1987; Nicolleau & Mathieu 1994). It is believed that the fractal dimension of a line develops from the smallest turbulence eddies to the largest (Villermaux & Gagne 1994), but cases of practical interest concern a blob of concentration that is three-dimensional objects or sections of such objects and the role of turbulence eddies in the development of the fractal dimension of these objects has received less attention. In terms of engineering applications, if surfaces are relevant to propagation flames and spark engines, compression ignition engines rely on good volume mixing. Can we find any useful relation between what we know of the fractal dimension of the line and those of the surface and volume? We try to answer that question using kinematic simulation to track particles and measure fractal dimensions of material lines, surfaces and volumes and of a blob of particles evolving in a turbulence field. Kinematic simulations provide realizations of the Lagrangian field, a necessary step as there is no possibility of measuring fractal dimensions from mean quantities. By contrast to direct numerical simulation, they also provide large-Reynolds-number computations or, more exactly, large ratios of inertial range scales, the very range where the fractal dimension is to develop.

The paper is organized as follows: this first section introduces the basics of kinematic simulation and particle tracking. Section 2 deals with the line, § 3 with the plane and § 4 with the volume. Section 5 complements § 4 with the study of an iso-scalar object. Finally, § 6 concludes this paper.

1.1. Kimematic simulation

Kinematic simulations (KS) are Lagrangian models of turbulent diffusion based on kinematically simulated turbulent velocity fields which are non-Markovian (not Diraccorrelated in time), incompressible and consistent with up to second-order statistics of the turbulence such as energy spectra. (See for instance Fung *et al.* (1992) for more details on the assumptions underlying KS.)

Kinematic simulations can reproduce detailed statistics of the Lagrangian velocity field such as flatness factors of Lagrangian relative velocities (Malik & Vassilicos 1999). By comparison to a Wiener process which causes fluid element pairs to separate in Lagrangian models of relative diffusion based on Langevin-type equations, the mechanism by which fluid element pairs separate in KS might be comparable to that in turbulent flows.

In practice, the KS approach relies on the integration of

$$\frac{\mathrm{d}x}{\mathrm{d}t} = u(x, t),\tag{1.1}$$

where x is the position of the fluid particle and u a turbulent-like Eulerian velocity field. Statistics are then performed on the trajectories. Incompressibility is enforced in the construction of u and the energy spectrum is prescribed according to the type of turbulence considered.

KS can be used to track particles with inertia (Fung, Hunt & Perkins 2003) and in some cases it can be extended to no isotropic turbulence (Nicolleau & Vassilicos 2000), but here we will only consider fluid particles released in a three-dimensional isotropic turbulence.

If u(x, t) is known, solving (1.1) is straight forward; but solving u(x, t) at every point and time can be difficult. Because of the computational expense of DNS, kinematic simulations have been proposed to simulate Lagrangian properties of turbulent flow fields. In KS, random flow fields are generated whose statistics agree with values obtained from experimental measurements or other reliable numerical simulations. KS use an analytical formula for u(x, t), therefore they are not grid-based and no interpolation of the velocity field is needed.

In this paper, we use a three-dimensional KS similar to that of Nicolleau & Yu (2004). The Eulerian velocity field used in (1.1) is generated as a sum of random Fourier modes. Incompressibility is enforced by construction of the velocity field in every realization. The energy spectrum is prescribed to take a -5/3 power law form (see also Fung *et al.* 1992; Elliott & Majda 1996; Fung & Vassilicos 1998; Malik & Vassilicos 1999; Nicolleau & Vassilicos 2003).

1.2. The velocity field

As in Nicolleau & Yu (2004), our three-dimensional KS velocity field is given as a sum of N random Fourier modes, i.e.

$$\boldsymbol{u}(\boldsymbol{x},t) = \sum_{n=1}^{N} (\boldsymbol{a}_n \times \widehat{\boldsymbol{k}}_n) \cos(\boldsymbol{k}_n \cdot \boldsymbol{x} + \omega_n t) + (\boldsymbol{b}_n \times \widehat{\boldsymbol{k}}_n) \sin(\boldsymbol{k}_n \cdot \boldsymbol{x} + \omega_n t), \quad (1.2)$$

 \hat{k}_n defined as $\hat{k}_n = k_n/|k_n|$ is a random unit vector so that

$$\mathbf{k}_{n} = |\mathbf{k}_{n}| \hat{\mathbf{k}}_{n} = |\mathbf{k}_{n}| \begin{pmatrix} \sin \theta_{n} \cos \phi_{n} \\ \sin \theta_{n} \sin \phi_{n} \\ \cos \theta_{n} \end{pmatrix}, \tag{1.3}$$

where $\theta_n \in [0, \pi]$ and $\phi_n \in [0, 2\pi]$ are picked randomly in each mode and realization. a_n and b_n are random and uncorrelated vectors with their amplitudes being chosen according to a prescribed power law energy spectrum E(k), i.e.

$$|\mathbf{a}_n|^2 = |\mathbf{b}_n|^2 = \frac{2}{3}E(k_n)\Delta k_n$$
 (1.4)

and

$$E(k) = \frac{u_0^2}{k_1} \left(\frac{k}{k_1}\right)^{-5/3} \quad \text{for } k_1 \leqslant k \leqslant k_N,$$

$$E(k) = 0 \quad \text{otherwise.}$$

$$(1.5)$$

Typical turbulence parameters we vary are the integral length scale

$$L = \frac{3\pi}{4} \frac{\int_{k_1}^{k_N} E(k)k^{-1} dk}{\int_{k_1}^{k_N} E(k) dk}$$
(1.6)

in the limit of large Reynolds numbers (i.e. $k_N \to \infty$)

$$L \simeq \frac{3\pi}{10} \frac{1}{k_1} = \frac{3}{20} L_1,$$

the turbulent velocity fluctuation intensity, defined by

$$u' = \sqrt{\frac{2}{3}} \int E(k) \, \mathrm{d}k$$

note that

$$u' \simeq u_0$$

for large enough Reynolds numbers and the Kolmogorov length scale, defined by

$$\eta = \frac{2\pi}{k_N}.$$

Hence, in KS, rather than the Reynolds number, the natural parameter is the ratio $L_1/\eta = k_N/k_1$ which is input data of the computation. An order of magnitude for the Reynolds number (*Re*) can be obtained from the relation

$$Re \sim \left(\frac{L}{\eta}\right)^{4/3}$$
.

We will see later on how we can calibrate an equivalent Reynolds number for the KS. In this paper, the distribution of the wavenumber is geometric, i.e.

$$k_n = k_1 \left(\frac{k_N}{k_1}\right)^{(n-1)/(N-1)}$$
 (1.7)

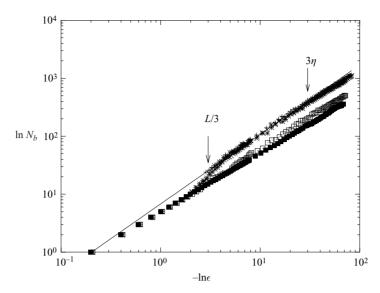


FIGURE 1. $\ln N_b$ as a function of $-\ln \epsilon$ for different values of λ . The box-counting was made at t=0.057L/u' for $L_1/\eta=178$. Different curves corresponds to +, $\lambda=0$; \times , $\lambda=0.5$; *, $\lambda=1$; \Box , $\lambda=5$; \blacksquare , $\lambda=20$. The line corresponds to the best fit curve between the two arrows, i.e. $y=8.7x^{1.199}$.

It is possible to introduce a frequency ω_n that determines the unsteadiness associated with the *n*th wavemode. Malik & Vassilicos (1999) chose it to be proportional to the eddy-turnover time of the *n*th wavemode, i.e.

$$\omega_n = \lambda \sqrt{k_n^3 E(k)},\tag{1.8}$$

where λ is the unsteadiness parameter and may be expected to be of the order of 1. It has been shown in isotropic turbulence (Malik & Vassilicos 1999) that for two-particle diffusion a significant number of statistical properties are insensitive to the unsteadiness parameter value in the range $0 \le \lambda \le 1$ in three-dimensional KS. In accordance with these results, we do not add any unsteadiness term to the KS. This is particularly justified here as we are not interested in the large-time random walk regime of the fluid particle diffusion. In this paper, particles are tracked for times smaller than 2/3 of the characteristic time $\tau_d = u'/L$. This result is further illustrated in figure 1. As discussed in §2, the fractal dimension is measured from the slope of the line fitting the points between the two arrows in figure 1. We repeat the results for $\lambda = 0$, 0.5, 1, 5 and 20. As can be seen, λ has no effect on these points provided that it is in the range [0, 1]. For $\lambda > 1$, the fractal dimension tends rapidly to 1 as λ increases, i.e. there is no turbulence structure. This is because the velocity field will be flapping so fast at all scales that the fluid elements do not have the time to experience the effect of eddying, streaming and straining flow structure (Malik & Vassilicos 1999).

It should also be noted from the constructed velocity field (1.2) that the coefficients of the *n*th Fourier mode are normal to k_n ensuring the incompressibility of the velocity field trajectory by trajectory.

In table 1 we summarize the different cases we run varying L and η .

1.3. Fractal dimension from kimematic simulation

Two-dimensional kinematic simulations were used by Fung & Vassilicos (1991) to compute the fractal dimension of a line. The use of KS allows us to reach large

								Δ_0/η for		
Case	u'	L	η	$\tau_d = L/u'$	k_N/k_1	$(k_N/k_1)^{4/3}$	Line	Plane	Cube	Iso-scalar
A	0.57	1.21	0.72	2.12	8.74	18	3.6×10^{-4}			
В	0.57	1.14	0.46	2.00	13.77	33	1.1×10^{-3}			
C	0.57	1.05	0.17	1.84	36	120	2.9×10^{-3}	0.06		6×10^{-3}
D	0.57	1.00	6.28×10^{-2}	1.76	100	464	8.0×10^{-3}	0.16	0.16	
E	0.57	0.99	3.53×10^{-2}	1.74	178	1000	1.4×10^{-2}	0.28	0.28	2×10^{-2}
F	0.57	0.98	2.10×10^{-2}	1.72	299	2000	2.4×10^{-2}	0.48		
G	0.57	0.97	1.25×10^{-2}	1.71	503	4000	4.0×10^{-2}	0.80		
Н	0.57	0.97	6.25×10^{-3}	1.70	1000	10 000		1.60	1.60	1.6×10^{-1}

Table 1. Different KS case summary, Δ_0 is the initial distance separating two neighbouring points.

Reynolds numbers. In this paper, we are more interested in the development of the fractal dimension of a line or surface than in its final value. As shown by Villermaux & Gagne (1994), this evolution is linked to the turbulence scales existing in the flow and this is a good validation for KS.

In practice, particles are released from their initial position at an initial time t_0 that for the sake of simplicity we set to 0, then we use KS to track the particle trajectories. The line discretization Δ_0 is fixed at t_0 , the corresponding values for Δ_0/η are reported in table 1. This initial distance is chosen small enough so that it remains small during the diffusion process for the fractal dimension to be accurate. In the case of the line, the r.m.s value of the distance between two neighbour particles is always at least 10 times smaller than the Kolmogorov length scale when we stop the computation. For other geometries, we could not afford that precision for all Reynolds numbers, but this was maintained at least for Re < 4000 and no particularities were observed in the two cases Re > 4000. At any time we can measure the fractal dimension of the set of points formed by the points where the particles are. We use the modified box-counting method of Buczkowski *et al.* (1998) to compute the fractal dimension. A case is shown in figure 2 where we plot the number of boxes N_b as a function of the inverse of the size of the box $1/\epsilon$. There is a fractal dimension if N_b is a power law of ϵ , that is in a logarithmic plot:

$$\ln N_b = -D \ln \epsilon + C,$$

where D is the fractal dimension. Figure 2 is representative of our results, for all fractal dimensions that we measured we observed the power law over more than 1 decade or a minimum range of $[L/3, 3\eta]$.

1.4. Evolution of an iso-scalar field

We can also use kinematic simulation to predict the evolution of a blob of concentration released in a turbulent velocity field and compute its fractal dimension as a function of time.

We use the method developed in (Flohr & Vassilicos 2000) to obtain concentrations as functions of space and time when molecular diffusion is neglected. This is studied in § 5.

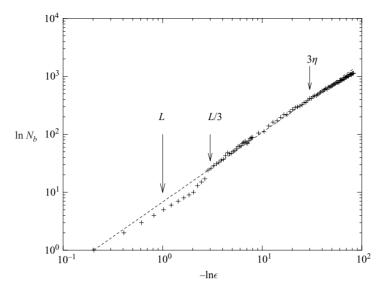


FIGURE 2. Precision of the box-counting method used in the computation of the fractal dimension. $\ln N_b$ as a function of $-\ln \epsilon$ at t = 0.057 L/u' for $L_1/\eta = 178$.

2. Fractal dimension of an initially one-dimensional line

The development of a fractal line was studied in (Nicolleau 1996); numerical results from a large eddy simulation were compared to experiments and theory from Villermaux & Gagne (1994). A general formula was proposed for the fractal dimension of the line D_l :

$$\frac{D_l - 1}{0.088Re^{1/2}} = \frac{t}{\tau_d},\tag{2.1}$$

where $\tau_d = L/u'$ is the turnover time. However, this was only validated for a limited range of Reynolds numbers and the numerical method then used was an LES which by construction does not resolve small-scale turbulence.

However, two-particle statistics are very significantly influenced by the entire range of flow structures (see e.g. Batchelor 1952). So, it is important to validate (2.1) with large Reynolds numerical experiments that involve large ratios of length scales and KS can do that.

Initially, the particles are released in the horizontal plane z = -0.25L on a line from point (-2.5L, 0.25L) to point (2.5L, 0.25L) as shown in figure 3. The parameters of the different turbulences considered are reported in table 1.

In figure 4, we plot $(D_l - 1)/0.088Re^{0.5}$ as a function of t/τ_d for experimental, LES and KS results. KS results in figure 4 correspond to the cases A, B, C, D, E, F and G described in table 1. For experimental cases, we use for the Reynolds numbers the values provided in Villermaux & Gagne (1994). For KS, we define the Reynolds number as

$$Re = 30.25 \left(\frac{L}{\eta}\right)^{4/3} = 2.61 \left(\frac{L_1}{\eta}\right)^{4/3}.$$
 (2.2)

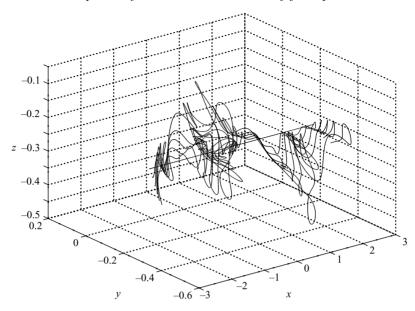


FIGURE 3. Evolution of a line embedded in turbulence as a function of time.

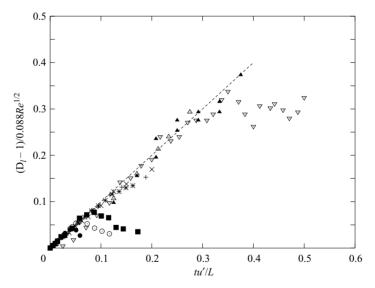


FIGURE 4. Evolution of the normalized fractal co-dimension of a line $(D_l-1)/0.088Re^{1/2}$ as a function of t(u'/L): KS for $(L_1/\eta)^{4/3}=18$ (+), 33 (×), 120 (*), 464 (\square), 1000 (\blacksquare), 2000 (\bigcirc) and 4000 (\bullet); Villermaux's experiment Re=18 (\triangle) and 33 (\triangle); LES for Re=120 (∇).

This is because in the demonstration for (2.1), what matters is the range of scales over which the fractal process occurs. This range is the range over which the spectral -5/3 power law is observed, that is $[L_1, \eta]$ in the case of KS. Whereas for experimental spectra, the power law $k^{-5/3}$ is observed over a range shorter than $[L, \eta]$. So for the same values of L and η , KS have a wider range of scales over which the fractal dimension can develop and we have to account for this difference. In (2.2), we define the KS Reynolds number such that the line results match the experimental curves

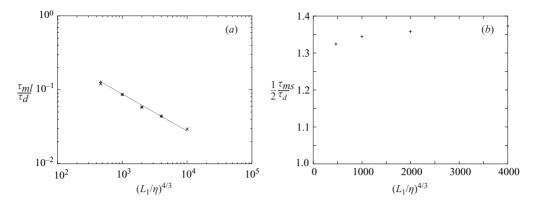


FIGURE 5. (a) +, non-dimensional time τ_{ml}/τ_d at which the maximum fractal dimension of the line is obtained as a function of $(L_1/\eta)^{4/3}$; ×, re-scaled non-dimensional time $(\tau_{ms}/\tau_d)/2$ at which the maximum fractal dimension of the square is obtained as a function of $(L_1/\eta)^{4/3}$ (see § 3.2). Interpolating line is $\tau_{ml}/\tau_d = 2.77(L_1/\eta)^{-2/3}$. (b) Maximum fractal dimension D_{max} reached by the line as a function of $(L_1/\eta)^{4/3}$.

from Villermaux & Gagne (1994). From now on, Reynolds numbers associated to a KS will use definition (2.2).

We observe that:

- (i) The line's fractal dimension obeys (2.1) with *Re* given by (2.2). It even catches the theoretical curve at small times better than the lines computed with LES. This is because the turbulence structures acting at small times have the smallest length scales and are the ones most likely to be influenced by the LES subgrid.
 - (ii) KS predicts an asymptotic value $D_l \simeq 1.37$ (see figure 5b).
- (iii) Equation (2.1) is still valid for large Reynolds numbers (up to $L_1/\eta = 503$) and figure 5b validates the fact that the time necessary to reach the asymptotic value $D_l \simeq 1.37 \ \tau_{ml}$ is proportional to $1/\sqrt{Re}$. With KS we find

$$\tau_{ml} = 2.77 \left(\frac{\eta}{L_1}\right)^{2/3} \frac{L}{u'} = 0.81 \left(\frac{\eta}{L}\right)^{2/3} \frac{L}{u'} \simeq \tau_{\eta}.$$
(2.3)

Having the line's maximum dimension reached in such a short time may be surprising but, as a comparison, if we put the obvious upper bound $D_l = 3$ in (2.1) then we obtain:

$$t(D_l = 3) = 22.7\tau_n$$
.

Hence, from the multiplicative approach adopted in Villermaux & Gagne (1994), the maximum fractal dimension has to be reached by few Kolmogorov time scales. Though there is no way to know this value from this theory. Earlier works by Meneveau & Sreenivasan (1990) (Sreenivasan, Ramshankar & Meneveau 1989) propose $1.33 \le D_l \le 1.36$. Another approach by Queiros-Conde (1999, 2000) using the concept of entropic skins leads to the same order of magnitude for τ_{ml} .

(iv) The line's dimension reaches a maximum value and then decreases. The decrease is due to the decrease in the resolution of the line at large times. The number of points discretizing the line is fixed at t = 0, therefore owing to particle pair separation the line's resolution cannot be maintained for times larger than τ_{ml} .

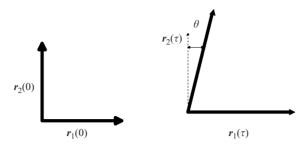


FIGURE 6. Shear and strain of an elementary square.

3. Fractal dimension of an initially two-dimensional surface

3.1. Theoretical analysis

Equation (2.1) was derived for a line using one-dimensional arguments. It was mainly derived from covering the line with segments and using the relation:

$$\epsilon \simeq \frac{\delta u(r)^3}{r},\tag{3.1}$$

where ϵ is the turbulence dissipation rate, $\delta u(r)$ the average velocity difference over a structure of size r (see e.g. Mathieu & Scott 2000, for the derivation of (3.1)). To generalize this result we investigate the fractal dimension of a two-dimensional object. Particles are released at t=0 from an horizontal plane at z=-0.1L on a square of size L see figure 7. The Villermaux & Gagne (1994) demonstration can easily be generalized to a plan. The difference in velocity at two points separated by a distance r is written as

$$\delta u(r) = f\left(\frac{r}{\eta}\right) (\epsilon r)^{1/3},\tag{3.2}$$

with

$$f\left(\frac{r}{\eta}\right) \to 1 \qquad \text{if } \frac{r}{\eta} \gg 1,$$

$$f\left(\frac{r}{\eta}\right) \to \left(\frac{r}{\eta}\right)^{2/3} \quad \text{if } \frac{r}{\eta} < 1.$$

$$(3.3)$$

A convenient form is

$$f\left(\frac{r}{\eta}\right) = 1 - \exp\left(-(r/\eta)^{2/3}\right). \tag{3.4}$$

If we consider the initial plan square of area A_0 , it can be covered with elementary squares of area $a_0 = |\mathbf{r}_1 \times \mathbf{r}_2|$. After a small interval of time τ each elementary square becomes distorted (figure 6) and the area of the distorted element is now

$$a(\tau) = |\mathbf{r}_1(\tau) \times \mathbf{r}_2(\tau)| = r_1(\tau)r_2(\tau)\cos\theta(\tau) = r_1(\tau)r_2(\tau)\left\{1 - \frac{1}{2}\left(\frac{\mathrm{d}r_2}{\mathrm{d}r_1}\frac{1}{r_2}\tau\right)^2\right\}, \quad (3.5)$$

that is at first order in τ

$$a(\tau) = (r_1(0) + \delta u_1(0)\tau) \times (r_2(0) + \delta u_2(0)\tau))$$
(3.6)

or as $|\mathbf{r}_2(0)| = |\mathbf{r}_1(0)| = r_0 = a_0^{1/2}$

$$a(\tau) \simeq a_0 + \left(\frac{\partial u_1}{\partial x_1}(0)r_0^2 + \frac{\partial u_2}{\partial x_2}(0)r_0^2\right)\tau = a_0 \left\{1 + \left(\frac{\partial u_1}{\partial x_1}(0) + \frac{\partial u_2}{\partial x_2}(0)\right)\tau\right\}. \tag{3.7}$$

This is where the plane development differs from the lines. Here we have to take into account the continuity equation

$$\frac{\partial u_1}{\partial x_1} + \frac{\partial u_2}{\partial x_2} + \frac{\partial u_3}{\partial x_3} = 0. \tag{3.8}$$

The stretchings along r_1 and r_2 have to be accounted together. Apart from that constraint, if we set

$$\alpha = \frac{\partial u_1}{\partial x_1}(0) + \frac{\partial u_2}{\partial x_2}(0) = \beta \frac{1}{r_0} \delta u_0, \tag{3.9}$$

we can generalize the approach used in Villermaux & Gagne (1994) for a line to the plane: equation (3.7) becomes

$$a(\tau) \simeq a_0 + \beta \delta u_0 r_0 \tau. \tag{3.10}$$

The total area of the square is then

$$A(\tau) = N_0 a(\tau) = N_0 (a_0 + \beta \delta u_0 r_0 \tau),$$

where N_0 is the initial number of elementary squares of area a_0 needed to cover the square at initial time t = 0. That is if we use equation (3.2),

$$A(\tau) = N_0 \left(a_0 + \beta f \left(\frac{r_0}{\eta} \right) \epsilon^{1/3} r_0^{4/3} \tau \right). \tag{3.11}$$

If we do the covering at time τ , we will need

$$N_{\tau}(a_0) = \frac{A(\tau)}{a_0} = N_0 \left(1 + \beta f\left(\frac{r_0}{\eta}\right) \epsilon^{1/3} r_0^{-2/3} \tau \right)$$

of such elementary squares. For an interval of time t, this mechanism is reproduced t/τ times so that:

$$N_t(a_0) = N_0 \left(1 + \beta f\left(\frac{r_0}{\eta}\right) \epsilon^{1/3} r_0^{-2/3} \tau \right)^{t/\tau}. \tag{3.12}$$

The dimension of the object is defined as

$$D_s(t) = -\left. \frac{\mathrm{d} \ln(N_t(a_0))}{\mathrm{d} \ln(r_0)} \right|_{r_0 = \eta}$$
(3.13)

with $\tau = \tau_{\eta}$. Using (3.4) we have:

$$D_s = 2 + \frac{2}{3} \frac{\beta}{1+\beta} \frac{e-2}{e-1} \frac{t}{\tau_n},$$
 (3.14)

or using the relation $\tau_{\eta} = (L/u')(\eta/L)^{2/3}$

$$D_s = 2 + \frac{2}{3} \frac{\beta}{1+\beta} \left(\frac{1-2/e}{1-1/e} \right) \left(\frac{L}{\eta} \right)^{2/3} t \frac{L}{u'}. \tag{3.15}$$

Relations (3.14) and (3.15) cannot predict the maximum fractal dimension and are, of course, valid only up to that maximum dimension that is for small times.

The plane deformation is a three-dimensional process constrained by the continuity equation, but we can try to set some boundaries for the value of β . According to (3.8), there is at least one positive and one negative value for $\partial u_i/\partial x_i$. Betchov (1956) has shown that, on average, there are two positive values and one negative. Though in each particular realization of the velocity field there can be two negative values, such a situation would lead to the formation of an elongated one-dimensional structure and a smaller area and fractal dimension. We can first discard these cases and use the average picture where there are two positive and one negative values for $\partial u_i/\partial x_i$, this will provide an upper bound for β and the fractal dimension. Let us set

$$\frac{\partial u_3}{\partial x_3} < \frac{\partial u_2}{\partial x_2} < \frac{\partial u_1}{\partial x_1}. (3.16)$$

There are three possible configurations:

(i) All the stretching effects on the surface are positive i.e. the surface is subjected to

$$\alpha_i = \frac{\partial u_1}{\partial x_1} + \frac{\partial u_2}{\partial x_2}. (3.17)$$

(ii) There is one negative stretching effect and the second one is the larger of the positive stretching effects:

$$\alpha_{ii} = \frac{\partial u_1}{\partial x_1} + \frac{\partial u_3}{\partial x_3}. (3.18)$$

(iii) The second one is the smaller of the positive stretching effects:

$$\alpha_{iii} = \frac{\partial u_2}{\partial x_2} + \frac{\partial u_3}{\partial x_3}. (3.19)$$

In addition to the continuity equation, we also have the relation

$$\frac{\delta u_0^2}{r_0^2} = \left(\frac{\partial u_1}{\partial x_1}\right)^2 + \left(\frac{\partial u_2}{\partial x_2}\right)^2 + \left(\frac{\partial u_3}{\partial x_3}\right)^2. \tag{3.20}$$

In case (i) (3.20) can be re-written as

$$\frac{\delta u_0^2}{r_0^2} = \left(\frac{\partial u_1}{\partial x_1}\right)^2 + \left(\frac{\partial u_2}{\partial x_2}\right)^2 + \left(\frac{\partial u_1}{\partial x_1} + \frac{\partial u_2}{\partial x_2}\right)^2,\tag{3.21}$$

that is

$$\frac{\delta u_0^2}{r_0^2} = 2\alpha_i^2 - 2\frac{\partial u_1}{\partial x_1}\frac{\partial u_2}{\partial x_2}$$

or

$$\alpha_i^2 = \frac{1}{2} \frac{\delta u_0^2}{r_0^2} + \frac{\partial u_1}{\partial x_1} \frac{\partial u_2}{\partial x_2}.$$

Furthermore, in case (i) we have

$$0 \leqslant \frac{\partial u_2}{\partial x_2} \leqslant \frac{\partial u_1}{\partial x_1},$$

so that

$$0 \leqslant \frac{\partial u_2}{\partial x_2} \frac{\partial u_1}{\partial x_1} \leqslant \left(\frac{\partial u_1}{\partial x_1}\right)^2,$$

the upper bound is found for $\partial u_2/\partial x_2 = \partial u_1/\partial x_1$ and, in this case, a combination of (3.8) and (3.20) yields

$$\left(\frac{\partial u_1}{\partial x_1}\right)^2 = \frac{1}{6} \frac{\delta u_0^2}{r_0^2}.\tag{3.22}$$

So that

$$\frac{1}{\sqrt{2}} \frac{\delta u_0}{r_0} \leqslant \alpha_i \leqslant \sqrt{\frac{2}{3}} \frac{\delta u_0}{r_0}.$$
(3.23)

Similarly, in case (ii) (3.20) can be re-written as

$$\frac{\delta u_0^2}{r_0^2} = \left(\frac{\partial u_1}{\partial x_1}\right)^2 + \left(\frac{\partial u_3}{\partial x_3}\right)^2 + \left(\frac{\partial u_1}{\partial x_1} + \frac{\partial u_3}{\partial x_3}\right)^2,\tag{3.24}$$

that is

$$\frac{\delta u_0^2}{r_0^2} = 2\alpha_{ii}^2 - 2\frac{\partial u_1}{\partial x_1}\frac{\partial u_3}{\partial x_3}$$

or

$$\alpha_{ii}^2 = \frac{1}{2} \frac{\delta u_0^2}{r_0^2} + \frac{\partial u_1}{\partial x_1} \frac{\partial u_3}{\partial x_3}.$$
 (3.25)

Furthermore, in case (ii) we have

$$\left(\frac{\partial u_1}{\partial x_1}\right)^2 \leqslant \left|\frac{\partial u_1}{\partial x_1}\frac{\partial u_3}{\partial x_3}\right| \leqslant \left(\frac{\partial u_3}{\partial x_3}\right)^2,$$

the upper bound is found for $\partial u_1/\partial x_1 = -\partial u_3/\partial x_3$ and $\partial u_2/\partial x_2 = 0$ so that in this case

$$\left(\frac{\partial u_3}{\partial x_3}\right)^2 = \frac{1}{2} \frac{\delta u_0^2}{r_0^2}.$$

The lower bound is found for $\partial u_1/\partial x_1$ minimum, that is $\partial u_1/\partial x_1 = \partial u_2/\partial x_2$, and we can use (3.22). As α_{ii} and $(\partial u_1/\partial x_1)(\partial u_3/\partial x_3)$ are negative, (3.25) leads to

$$-\frac{1}{\sqrt{6}}\frac{\delta u_0}{r_0} \leqslant \alpha_{ii} \leqslant 0. \tag{3.26}$$

Case (iii) is similar to (ii) and we can deduce

$$\alpha_{iii}^2 = \frac{1}{2} \frac{\delta u_0^2}{r_0^2} + \frac{\partial u_2}{\partial x_2} \frac{\partial u_3}{\partial x_3}$$
 (3.27)

and

$$0 \leqslant \left| \frac{\partial u_2}{\partial x_2} \frac{\partial u_3}{\partial x_3} \right| \leqslant \left| \frac{\partial u_1}{\partial x_1} \frac{\partial u_3}{\partial x_3} \right|,$$

but now the upper bound is found for $\partial u_2/\partial x_2$ maximum, that is $\partial u_2/\partial x_2 = \partial u_1/\partial x_1$, in this case, we have already seen in (3.22) that $(\partial u_2/\partial x_2)^2 = (\delta u_0^2/r_0^2)/6$ so that

$$\left(\frac{\partial u_3}{\partial x_3}\right)^2 = \frac{2}{3} \frac{\delta u_0^2}{r_0^2}.$$

As α_{iii} and $(\partial u_1/\partial x_1)(\partial u_3/\partial x_3)$ are negative, (3.27) leads to

$$-\frac{1}{\sqrt{2}}\frac{\delta u_0}{r_0} \leqslant \alpha_{iii} \leqslant -\frac{1}{\sqrt{6}}\frac{\delta u_0}{r_0}.$$
 (3.28)

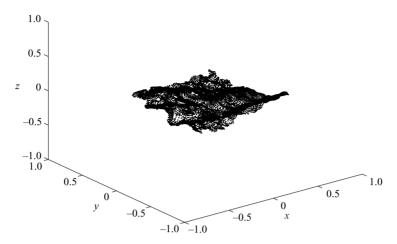


FIGURE 7. Evolution of a set of particles released from an horizontal square in the plane z = -0.1L, turbulence case E at time t = 0.09L/u'.

If all the three cases (i), (ii) and (iii) were as likely to occur, then an average value for α would be

$$\overline{\alpha} = \frac{1}{3} (\langle \alpha_i \rangle + \langle \alpha_{ii} \rangle + \langle \alpha_{ii} \rangle),$$

and then, using previous results, we can give an upper and lower bound for $\overline{\alpha}$

$$-\frac{1}{3\sqrt{6}}\frac{\delta u_0}{r_0} \leqslant \overline{\alpha} \leqslant \frac{1}{3\sqrt{6}}\frac{\delta u_0}{r_0},\tag{3.29}$$

that is in terms of K defined as follows:

$$D_s = 2 + K0.088 \left(\frac{L}{\eta}\right)^{2/3} t \frac{L}{u'} - 0.23 \leqslant K \leqslant 0.23.$$
 (3.30)

However, this picture is unlikely, Batchelor (1952) and Girimaji & Pope (1990) showed that elementary surfaces align with the directions of maximum strain, hence case (i) is much more likely to occur than cases (ii) or (iii). We obtain an upper bound of all the possibilities when only (i) is present, which leads to

$$0.83 < K < 0.90. (3.31)$$

So even in the best case for area increase, the increase is smaller than for the lines by at least 10%. From our KS results we find $K \simeq 0.5$, indicating something in-between the two extreme cases total isotropic distribution of the elementary squares (3.30) or total alignment (3.31).

3.2. KS analysis of a plane

We use KS to compute the fractal dimension of a set of particles released on a square at t=0. The initial square is in the plane z=-0.1L centred on (0,0,0) and has a side length of L. Each particle from the square is tracked so that we can follow the evolution of the square as a function of time. Figure 7 shows this evolution at $t=0.15\tau_d$ for the case referred to as E in table 1.

We can then measure the fractal dimension of the set of particles using our box-counting algorithm. In figure 8, we plot the non-dimensional fractal co-dimension

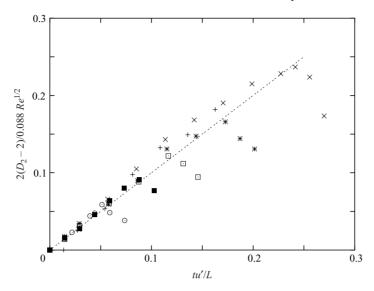


FIGURE 8. Evolution of the normalized fractal co-dimension $2(D_2-2)/0.088Re^{1/2}$ of an initially plane square as a function of tu'/L. Different ratios are: +, $L_1/\eta = 36$; \times , 100; *, 178; \square , 299; \blacksquare , 503; \odot , 1000.

 $2(D_2-2)/0.088Re^{1/2}$ as a function of the non-dimensional time tu'/L varying the Reynolds numbers. All the curves collapse, indicating a universal law similar to (2.1):

(i) The surface fractal dimension of an initial plane obeys (3.32)

$$\frac{D_s - 2}{0.088Re^{1/2}} = \frac{1}{2} \frac{t}{\tau_d},\tag{3.32}$$

where Re is still defined by (2.2), that is

$$D_s = 2 + 0.044Re^{1/2}t\frac{u'}{L} (3.33)$$

or

$$D_s = 2 + 0.071 \left(\frac{L_1}{\eta}\right)^{2/3} t \frac{u'}{L}.$$

This is verified for Reynolds numbers up to $L_1/\eta = 1000$.

- (ii) KS predicts the asymptotic value $D_s \simeq 2.4$ (figure 9).
- (iii) In figure 5, we plot $\tau_{ms}/2$ as a function of $(L_1/\eta)^{4/3}$, where τ_{ms} is the time necessary to reach the maximum fractal dimension for the square $D_s \simeq 2.4$. We observe that

$$\tau_{ml} = \frac{1}{2}\tau_{ms}.\tag{3.34}$$

(iv) As in the case of the line, we can see that the surface resolution decreases after τ_{ms} , resulting in a decrease of the surface dimension.

From all these results we can conclude that the plane surface dimension still follows the pattern underlying (2.1).

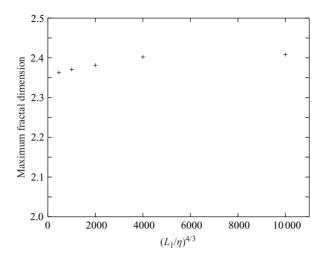


FIGURE 9. Maximum fractal dimension reached by our KS for the square as a function of $(L_1/\eta)^{4/3}$.

We can deduce the formula for the area of the initial square as a function of time, by definition of the fractal dimension:

$$A(t) \simeq L_s^2 \left(\frac{L_s}{\eta}\right)^{D_s - 2} = L_s^2 \left(\frac{L_s}{\eta}\right)^{0.071(L_s/\eta)^{2/3}t(u'/L)},\tag{3.35}$$

where L_s is the smaller of L_1 and the size of the square.

4. Fractal dimension of an initial volume object

Investigating a volume leads to a very different picture. The mechanisms leading to the line and surface development rely on the two positive eigenvalues of the velocity tensor (Girimaji & Pope 1990). Whereas in the case of the volume, we have to take into account the three eigenvalues of the velocity tensor and in the case of an incompressible flow, the total volume has to be conserved.

We released particles from cubes of different size s and a sphere of diameter d=0.2L, use KS to track the particles and then measure the fractal dimension D_v of the set of particles as a function of time. For a three-dimensional object, there is both stretching and contraction and eventually the volume tends to contract to a sheet, as shown in figure 10.

We can apply our box-counting method to the cube to find the evolution of its fractal dimension as a function of time.

- (i) Here, because of the contraction of the cube, the fractal dimension is decreasing. In figure 11, we plot D_v the fractal dimension of what was initially a cube of size s as a function of tu'/L for different ratios $L_1/\eta = 100$, 178 and 1000 and different cube sizes s = 0.2L, 0.25L and 0.3L
- (ii) By contrast to the line and surface, we can see from figure 11 that the evolution of the fractal dimension of the three-dimensional object is independent of the Reynolds number but depends on the ratio s/L, that is, on the range of inertial scales embedded in the object. This is consistent with the results of Villermaux, Innocenti & Duplat (1998) and Villermaux & Innocenti (1999) on the iso-scalar section, as we will see in § 5. These authors experimentally studied the evolution of a

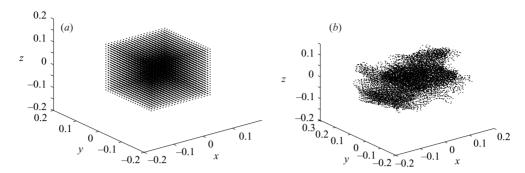


FIGURE 10. Evolution of a set of particles released from a cube in turbulence case E. (a) Initial cube, (b) particle cloud at time t = 0.17L/u'.

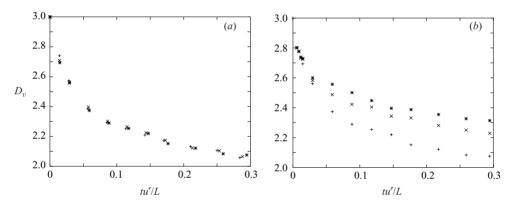


FIGURE 11. Evolution of the fractal dimension D_v of an initial cube as a function of tu'/L. (a) For a given cube size s=0.2L, the Reynolds number is varied; +, $L_1/\eta=100$; \times , 178; *, 1000. (b) For a given Reynolds number $L_1/\eta=1000$ the size of the cube is varied; +, s=0.2L; \times , s=0.25L; *, s=0.3L.

blob of concentration and concluded that the mixing time associated with the blob of concentration was independent of the Reynolds number, but a function of the size of the blob.

(iii) In figure 12, we plot $s(3 - D_v)/tu'$ as a function of tu'/L for different Reynolds numbers and different ratios s/L. With this latter normalization, and using a logarithmic plot, all the curves collapse onto a single line so that

$$s\frac{3-D_v}{tu'} = 0.25 \left(\frac{tu'}{L}\right)^{-2/3}. (4.1)$$

In this figure, we also plot, with the same normalization, the fractal dimension obtained when the source is a sphere of diameter d = 0.2L. The results are independent of the initial shape of the object sphere or cube. Furthermore, it is worth noting that the larger tu'/L, the better the collapse.

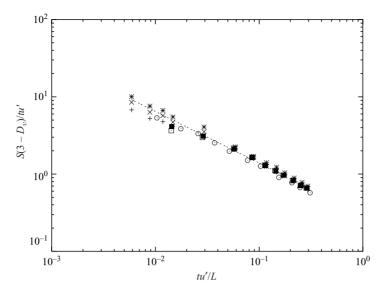


FIGURE 12. Re-scaled dimension $s(3-D_v)/tu'$ in logarithmic axes for all cases in figure 11. $L_1/\eta=1000$: +, s=0.2L; ×, s=0.25L; *, s=0.3L. s=0.2L: \Box , $L_1/\eta=100$; \blacksquare , $L_1/\eta=178$; spherical source with d=0.2L and $L_1/\eta=1000$. The fitting curve represented is $y=0.25x^{-2/3}$.

(iv) Equation (4.1) can be rearranged so that the fractal dimension of the initial cube D_v obeys

$$D_v = 3 - \frac{1}{4} \frac{L}{s} \left(\frac{tu'}{L} \right)^{1/3}. \tag{4.2}$$

(v) The fractal dimension D_v is found to decrease towards 2 as tu'/L and L/s increase.

5. Fractal dimension of an iso-scalar field

In practice, it is difficult to follow a three-dimensional object and most experimentalists look at iso-scalar surfaces (see, e.g. Lane-Serff 1993; Catrakis & Dimotakis 1996.) Villermaux & Innocenti (1999) made a detailed analysis of the evolution of the fractal dimension as a function of time.

Here, we study the evolution of a scalar whose initial concentration is

$$C(x,t) = 1 \quad \text{if } |x| < d/2,$$

$$C(x,t) = 0 \quad \text{otherwise.}$$
(5.1)

d is the source size. We use the method developed by Flohr & Vassilicos (2000) to obtain the points of the plane z = 0 such that C(x, t) = 1, as shown in figure 13. The scalar diffusion is neglected so that the concentration field is governed by

$$\frac{\partial C}{\partial t} + u_j \frac{\partial C}{\partial x_j} = 0.$$

With no diffusion term, we can use the method of characteristics: C(x, t) is constant on a particle trajectory and we propose to use kinematic simulation (KS) to predict particle trajectories. At time t and point x we construct the particle's trajectory backward in time in order to find its initial position. As KS relies on an analytical

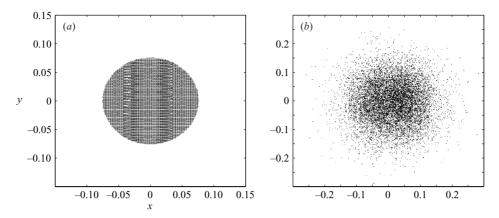


FIGURE 13. Evolution of the region of concentration c = 1 in the plane z = 0 as a function of time. (a) Initial concentration, (b) concentration c = 1 at time $t = 0.17\tau_d$.

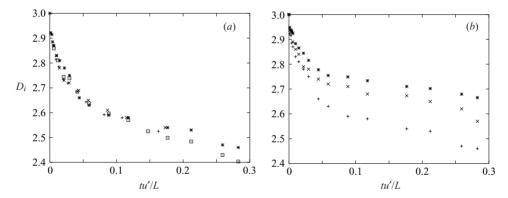


FIGURE 14. D_i as a function of tu'/L. (a) Different sources of a given size d=0.15; spherical source, (+) $L_1/\eta = 36$, (×) 178, (*) 1000 and cubical source, (-) $L_1/\eta = 1000$. (b) $L_1/\eta = 1000$, sources of different sizes; (+) d=0.15L, (×) 0.2L; (*) 0.25L.

formula for the Eulerian velocity field, there is no problem in reversing the tracking method. Then, the concentration at x and t is the concentration that was at t = 0 and x(0) the particle initial position:

$$C(x,t) = C(x(0),0).$$
 (5.2)

In practice, we compute the fractal dimension on a section that is the intersection of the fractal object with the plane z=0, then owing to isotropy, we assume that the fractal dimension of the fractal object embedded in the three-dimentional space is that of the section plus one. The advantage of this method is that while tracking the same number of points, we will obtain better resolution of the iso-scalar surface section. In figure 14 we show the fractal dimension as a function of the non-dimensional time tu'/L for different Reynolds numbers Re, cases C, E and H in table 1.

In figure 15 we plot in a logarithmic graph the normalized co-dimension $d(3 - D_i)/tu'$ as a function of tu'/L for case H reported in table 1 and varying the ratio d/L. We observe a good collapse of the different cases on a line indicating that $d(3 - D_i)/tu'$ is a universal power law of tu'/L. The law we find is $d(3 - D_i)/tu' = 0.13(tu'/L)^{-2/3}$,

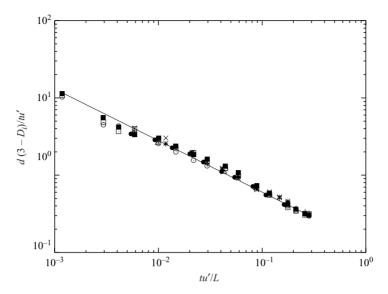


FIGURE 15. Logarithmic plot of the evolution of $d(3-D_i)/tu'$ as a function of tu'/L. Cubical source, $L_1/\eta = 1000$: +, s/L = 0.15; ×, s/L = 0.20; *, s/L = 0.25. Spherical source, $L_1/\eta = 1000$: \Box , d/L = 0.15; \blacksquare , d/L = 0.20; \bigcirc , d/L = 0.25. Spherical source, d/L = 0.15: \bullet , $L_1/\eta = 36$; \triangle , $L_1/\eta = 178$. The trend line is $y = 0.13x^{-2/3}$.

that is

$$D_i = 3 - 0.13 \left(\frac{tu'}{L}\right)^{1/3} \frac{L}{d}.$$
 (5.3)

This result has to be compared with (4.2) obtained for the cube. The two results are similar except for the coefficient 0.13 instead of 0.25. We should expect to find the same results when no diffusion is accounted for when considering the iso-scalar object. The discrepancy we find between the two coefficients is due to the method we use for computing the fractal dimension of the iso-scalar field. Tracking backward a complete three-dimensional field is too time consuming and we choose to consider only a section of the object, this may explain the ratio of 2 between the two coefficients. The assumption usually made that the dimension of the total object is that of a section plus one is not validated by our kinematic simulation.

It is worth commenting at this point on the form of (4.2) and (5.3) implying a different process from that involved in making the fractal dimension in lines and surfaces. As already mentioned, these equations are consistent with experimental results (Villermaux & Innocenti 1999) showing no dependence on the Reynolds number, but clear dependence on the source's size. The dependence on the ratio L/s is consistent with having L/u' as the characteristic time for the dimension's growth. Indeed, if we consider a box of size L according to (4.2), it will need a time L/u' to reach its full fractal potential, that is, the maximum fractal co-dimension $3-D_v$ over the range of scales it contains, η to L. A portion d/L of this box will need a much smaller time as it must reach its fractal potential over a smaller range of scales.

6. Conclusion

In this paper, we use kinematic simulation to track clouds of fluid particles from lines, planes and three-dimensional geometries. We then measure the evolution of their

fractal dimensions as functions of time. KS results for the line agree with previous experimental and numerical results. Dimensions of lines and planes vary linearly with time at least for times smaller than, or of the order of, the Kolmogorov timescale τ_n .

The fractal dimension D_s of a material surface obeys a law similar to that found for a material line:

$$D_s = 2 + 0.044 \frac{t}{\tau_{\eta}}.$$

This is observed up to a time $\tau_{ms} = 2\tau_{\eta}$ and a maximum dimension $D_s \simeq 2.4$. At any time $t < \tau_{ml}$, the surface fractal co-dimension's increase $(D_s - 2)$ is half that predicted for the line. The characteristic time for the dimension's growth is the Kolmogorov time micro-scale τ_n .

The fractal dimension of an initially three-dimensional object does not depend on the turbulence Reynolds number, but on the range of inertial scales it contains, that is, on the ratio L/s or L/d where s is the cube's size and d the sphere's diameter. The fractal dimension then obeys:

$$D_v = 3 - \frac{1}{4} \frac{L}{s} \left(\frac{tu'}{L} \right)^{1/3}.$$

The law is the same for a spherical or cubical source and the dimension's growth is governed by the turbulence large-scale characteristic time L/u'.

Similar properties are observed for the evolution of the dimension of a section of an iso-scalar field. This is consistent with the experimental work of Villermaux & Innocenti (1999). However, KS does not validate the usual assumption that the dimensions of a three-dimensional object can be obtained by adding 1 to the dimension of a section of this object.

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REFERENCES

BATCHELOR, G. K. 1952 The effect of homogeneous turbulence on material lines and surfaces. *Proc. R. Soc. Lond.* A **213**, 349.

Betchov, R. 1956 An inequality concerning the production of vorticity in isotropic turbulence. J. Fluid Mech. 1, 497–504.

BUCZKOWSKI, S., KYRIACOS, S., NEKKA, F. & CARTILIER, L. 1998 The modified box-counting method: analysis of some characteristic parameters. *Pattern Recog.* 31, 411–418.

CATRAKIS, H. J. & DIMOTAKIS, P. 1996 Mixing in turbulent jets: scalar measures and isosurface geometry. J. Fluid Mech. 317, 369–406.

ELLIOTT, F. W. & MAJDA, A. J. 1996 Pair dispersion over an intertial range spanning many decades. *Phys. Fluids* **8**, 1052–1060.

FLOHR, P. & VASSILICOS, J. C. 2000 Scalar subgrid model with flow structure for large-eddy simulations of scalar variances. *J. Fluid Mech.* 407, 315–349.

Fung, J. C. H., Hunt, J. C. R., Malik, N. A. & Perkins, R. J. 1992 Kinematic simulation of homogeneous turbulence by unsteady random Fourier modes. *J. Fluid Mech.* **236**, 281–317.

Fung, J. C. H., Hunt, J. C. R. & Perkins, R. J. 2003 Diffusivities and velocity spectra of small inertial particles in turbulent-like flows. *Proc. R. Soc. Lond.* A **459**, 445–493.

Fung, J. C. H. & Vassilicos, J. C. 1991 Fractal dimensions of lines in chaotic advection. *Phys. Fluids* A 3, 2725–2733.

Fung, J. C. H. & Vassilicos, J. C. 1998 Two-particle dispersion in turbulentlike flows. *Phys. Rev.* E **52**, 1677–1690.

GIRIMAJI, S. S. & POPE, S. B. 1990 Material element deformation in isotropic turbulence. J. Fluid Mech. 220, 427–458.

- GOULDIN, F. C. 1987 An application of fractals to modeling premixed turbulent flames. *Combust. Flame* **68**, 249–266.
- Lane-Serff, G. F. 1993 Investigation of the fractal structure of jets and plumes. *J. Fluid Mech.* 249, 521–534.
- MALIK, N. A. & VASSILICOS, J. C. 1999 A Lagrangian model for turbulent dispersion with turbulentlike flow structure: comparison with DNS for two-particle statistics. *Phys. Fluids* 11, 1572– 1580
- MATHIEU, J. & SCOTT, J. 2000 An Introduction to Turbulent Flow. Cambridge University Press.
- MENEVEAU, C. & SREENIVASAN, K. R. 1990 Interface dimension in intermittent turbulence. *Phys. Rev.* A 41, 2246–2248.
- NICOLLEAU, F. 1996 Numerical determination of turbulent fractal dimensions. *Phys. Fluids* **8**, 2661–2670
- NICOLLEAU, F. & MATHIEU, J. 1994 Eddy Break up model and fractal theory comparisons with experiments. *Intl J. Heat Mass Transfer* 37, 2925–2933.
- NICOLLEAU, F. & VASSILICOS, J. C. 2000 Turbulent diffusion in stably stratified non-decaying turbulence. J. Fluid Mech. 410, 123-146.
- NICOLLEAU, F. & VASSILICOS, J. C. 2003 Turbulent pair diffusion. Phys. Rev. Lett. 90, 245003.
- NICOLLEAU, F. & Yu, G. 2004 Two-particle diffusion and locality assumption. *Phys. Fluids* 16, 2309–2321.
- QUEIROS-CONDE, D. 1999 Géométrie de l'intermittence en turbulence développée. C. R. Acad. Sci. Paris 327 (Série II b), 1385–1390.
- QUEIROS-CONDE, D. 2000 Le modèle des peaux entropiques en turbulence développée. C. R. Acad. Sci. Paris 328 (IIb), 541–546.
- SREENIVASAN, K. R., RAMSHANKAR, R. & MENEVEAU, C. 1989 Mixing, entrainment and fractal dimensions of surfaces in turbulent flows. *Proc. R. Soc. Lond.* A **421**, 79–108.
- VILLERMAUX, E. & GAGNE, Y. 1994 Line dipersion in homogeneous turbulence: stretching, fractal dimensions and micromixing. *Phys. Rev. Lett.* **73**, 252–255.
- VILLERMAUX, E. & INNOCENTI, C. 1999 On the geometry of turbulent mixing. J. Fluid Mech. 393, 123–147.
- VILLERMAUX, E., INNOCENTI, C. & DUPLAT, J. 1998 Histogramme des fluctuations scalaires dans le mélange turbulent transitoire. C. R. Acad Sci. Paris 326 (IIb), 21–26.