



## Alumina doped Fe<sub>2</sub>O<sub>3</sub> foams by freeze-casting for redox cycling applications

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### ABSTRACT

Hydrogen is the next energy vector for a decarbonization society but industrial production is still methane-based. The Steam Iron Process (SIP) could provide a carbon-free production and safety storage option. Here, we show that a Fe<sub>2</sub>O<sub>3</sub>-3 wt% of Al<sub>2</sub>O<sub>3</sub> foams created by freeze-casting withstand 10 redox cycles at different temperatures with no reduction in performance or pore shrinking. The use of stearic acid as a dispersant agent/binder produces the porous structure enhancement of the foam and promotes the early reduction of the hematite phase during foam sintering. The Al<sub>2</sub>O<sub>3</sub> incorporation was detected as a solid solution in the Fe<sub>2</sub>O<sub>3</sub> phase at the particle surface. This result is relevant as correlated the positive values of the zeta potential observed. Freeze-casted foams could improve long-term redox performances combining a unique tailored interconnected pore structure with a specific chemical composition.

### 1. Introduction

Over recent years, the need for a clean and renewable energy source is undeniable. The concentration of greenhouse gases from the overuse of fossil fuels is causing a global emergency [1]. Hydrogen is an energy vector that could counterbalance this harmful effect as no CO<sub>2</sub> is emitted during its consumption. However, large-scale hydrogen production is still methane-based [2]. A green and cost-effective method for hydrogen production and storage must involve the use of renewable resources (e.g. biomass) [3] with pre-existing technologies such as the Chemical Looping Hydrogen (CLH) [4] or Steam-Iron Process (SIP) [5,6]. The SIP is a two-step process, where an iron oxide (oxygen carrier) is exposed to a reducing gas stream, such as ethanol [7,8] or bioethanol, to turn it into metal iron, then a steam flow re-oxidizes the metal to Fe<sub>3</sub>O<sub>4</sub> and produces pure hydrogen by splitting the water molecule, this process is repeated numerous until the iron oxide loses their redox capability. The use of bioethanol instead of most common methanol gas to produce hydrogen, reduces the operation temperatures and allows the revalorization of such renewable source [9,10].

Fe<sub>2</sub>O<sub>3</sub> (hematite) is an abundant and inexpensive raw material with attractive oxygen carrier capability due to its redox properties [11–13].

However, the redox performance is deeply affected by the deactivation phenomena due to the sintering process after numerous redox cycles at high temperature. To prevent the deactivation, hematite has been doped with CeO<sub>2</sub> [6], La<sub>2</sub>O<sub>3</sub> [14], CaO<sub>2</sub> [15,16], or Al<sub>2</sub>O<sub>3</sub> [17]. Al<sub>2</sub>O<sub>3</sub> additions are known to improve the cycle stability of Fe<sub>2</sub>O<sub>3</sub> [11] and stabilize the amount of H<sub>2</sub> generated during continuous operation [18], it also increases the mechanical properties at higher temperatures due to its higher Tamman temperature [19]. Several methods to incorporate the Al<sub>2</sub>O<sub>3</sub> into iron oxide particles have been studied, such as the mechanical mixing [20], impregnation [21], or co-precipitation [22]. Furthermore, Al<sub>2</sub>O<sub>3</sub> as an additive shows limited solubility into the iron oxides structures and neglected solubility in Fe. During reduction, Al<sub>2</sub>O<sub>3</sub> phase is consolidated and could form FeAl<sub>2</sub>O<sub>4</sub> (hercynite) at the oxidation step which reduces the redox performance of the oxygen carrier [23]. An option to counterbalance this effect could be to limit the conversion of the iron oxides to full metal [17].

A new approach has been recently proposed, to replace the use of powder in the fluidized-bed systems by structural porous materials as oxygen carriers [24–26]. Freeze-casting (FC) is a manufacturing technique devoted to produce structural porous materials with different pore sizes and morphologies [27,28]. But also, it is a cost-effective near net

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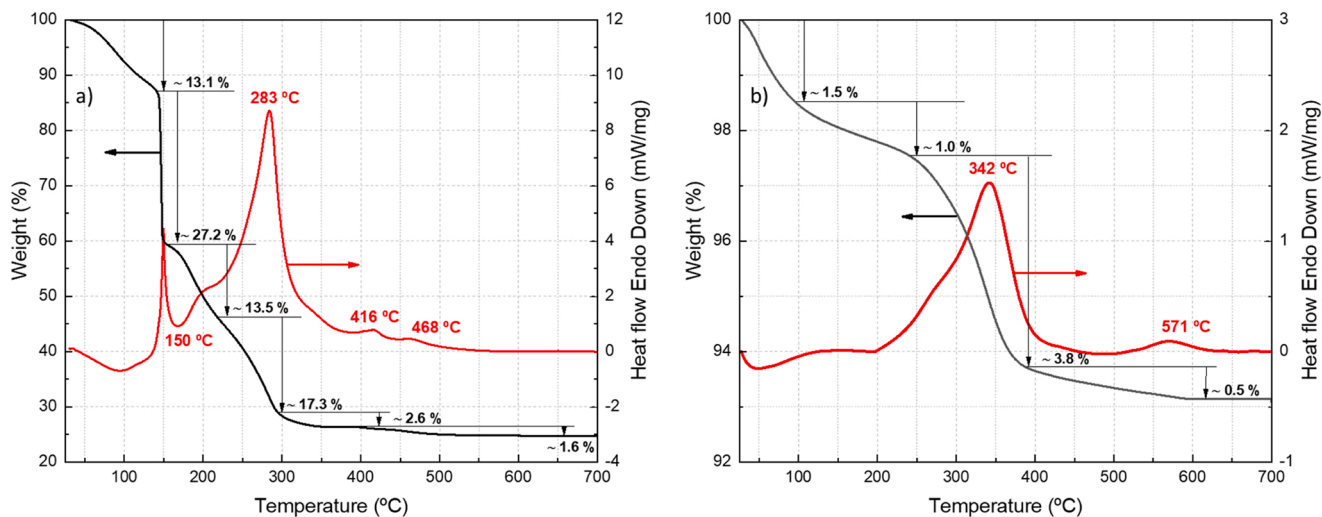


Fig. 1. TG (black lines) and DSC (red lines) curves of synthesized powder at different initial conditions: at gel form (a) and dried at 110 °C overnight (b). (For interpretation of the references to color in this figure legend, the reader is referred to the web version of this article.)

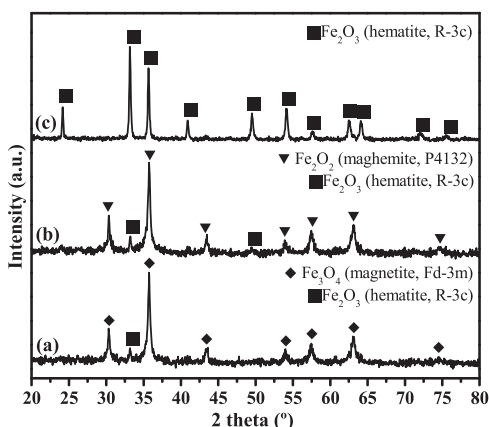


Fig. 2. XRD patterns of the synthesized powder (gel form) calcined at different temperatures: 170 °C (a), 350 °C (b) both for 2 h and 620 °C (c) for 6 h.

shaping (NNS) technology allowing foams fabrication in multiple sizes and shapes. However, pure Fe-foams manufactured by FC using water [29] and camphene-based [30,31] hematite slurries have shown a

significant modification of the pore structure after being subjected to several redox cycles. Authors have found a continuous reduction in the pore size due to the sintering of the Fe cell walls, which is especially critical when pores were under 30 μm in diameter [24]. Thus, the combination of an improved chemical formulation with the use of a highly interconnected pore structure with a high surface area could enhance the redox performance.

In this research, we have successfully manufactured Al<sub>2</sub>O<sub>3</sub> doped Fe<sub>2</sub>O<sub>3</sub> foams with an average pore size over 120 μm in diameter. The influences of the processing variables and the redox performance at different temperatures were studied. Redox cycles were conducted with a partial reduction step with hydrogen and an oxygen oxidation step to test the evolution of the pore structure with full reconversion to Fe<sub>2</sub>O<sub>3</sub>.

## 2. Experimental procedure

### 2.1. Powder synthesis

Doped Fe<sub>2</sub>O<sub>3</sub> powders with 3 wt% of Al<sub>2</sub>O<sub>3</sub> (named as Fe3Al) was synthesized using the citrate method previously described by Lorente et al. [32]. Briefly, 2 M aqueous solutions of selected metal nitrates (Fe (NO<sub>3</sub>)<sub>3</sub>·9H<sub>2</sub>O (98+% purity) and Al(NO<sub>3</sub>)<sub>3</sub>·9H<sub>2</sub>O (98% purity) with citric acid (99 +% purity) were mixed and stirred at 80 °C until a gel is

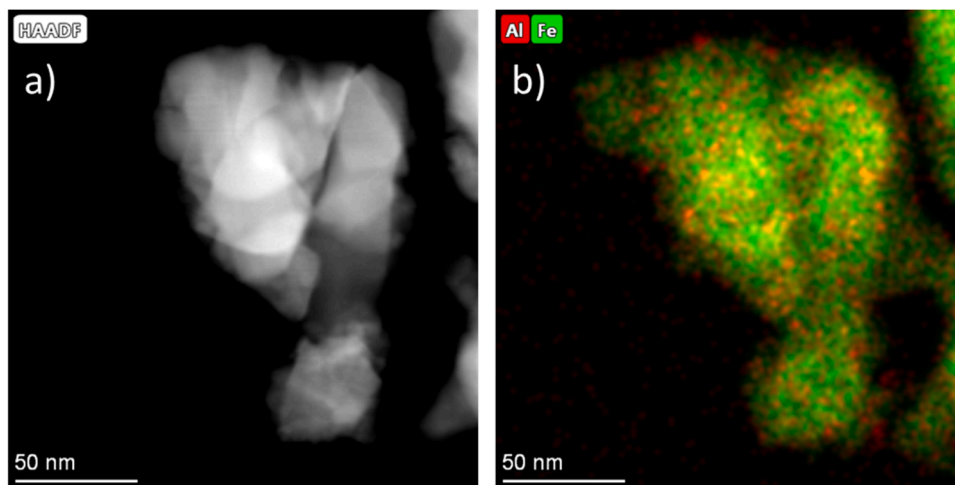


Fig. 3. High-Angle Annular Dark-Field (HAADF) image (a) and element distribution of Fe and Al by EDX analysis (b) of the Fe3Al calcined powder.

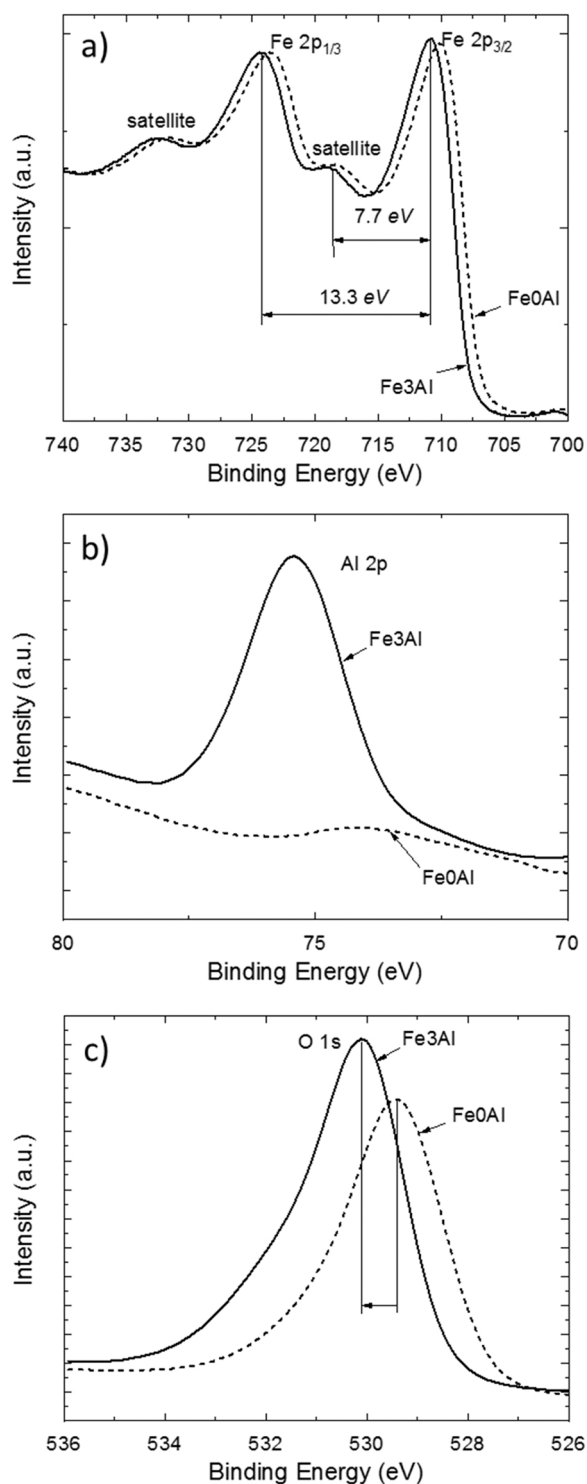


Fig. 4. High-resolution XPS spectra of Fe 2p (a), Al 2p (b), and O 1s (c) of the Fe3Al and FeOAl calcined powder after.

obtained. The molar ratio of citric acid to metal nitrates was set to 1 in the solution. The gels were dried overnight at 110 °C and calcined at 620 °C during 8 h. The synthesized powders were finally ball-milled for 24 h to reduce the particle size. All reactive agents were procured from Alfa Aesar™.

## 2.2. Foam manufacturing

Camphene (95% purity, Sigma Aldrich, Spain) slurries with 10 vol%

of Fe3Al powder loading were produced by ball milling at 60 °C for 24 h using 1, 2, or 3 wt% of stearic acid –SA– (98% purity, Sigma Aldrich, Spain) related to the powder load, as dispersant agent. The SA was added and mixed with the camphene for 30 min prior the powder was incorporated.

After the ball milling, camphene suspensions were poured into a copper base with PTFE walls mould of 30 mm in diameter by 15 mm in height preheated at 60 °C placed inside an incubator. Directional solidification was promoted by running water at 42.5 °C through the mould base and gradually reducing the incubator temperature at 0.2 °C·min<sup>-1</sup> until the complete sample solidification. Once demoulding, samples were subjected to a 3-day camphene sublimation process at ambient conditions under forced airflow, to later being heat-treated in air at 600 °C for 2 h for organic-specimen burn-out and 1100 °C for 2 h for particle sintering. To avoid crack formation during sintering, heating and cooling rates were set at 1 °C·min<sup>-1</sup> and 5 °C·min<sup>-1</sup>, respectively. Foam manufacturing procedure was based on a previous study [33]. Finally, sintered Fe3Al foams samples of approximately 12 mm in height and 24 mm in diameter were manufactured.

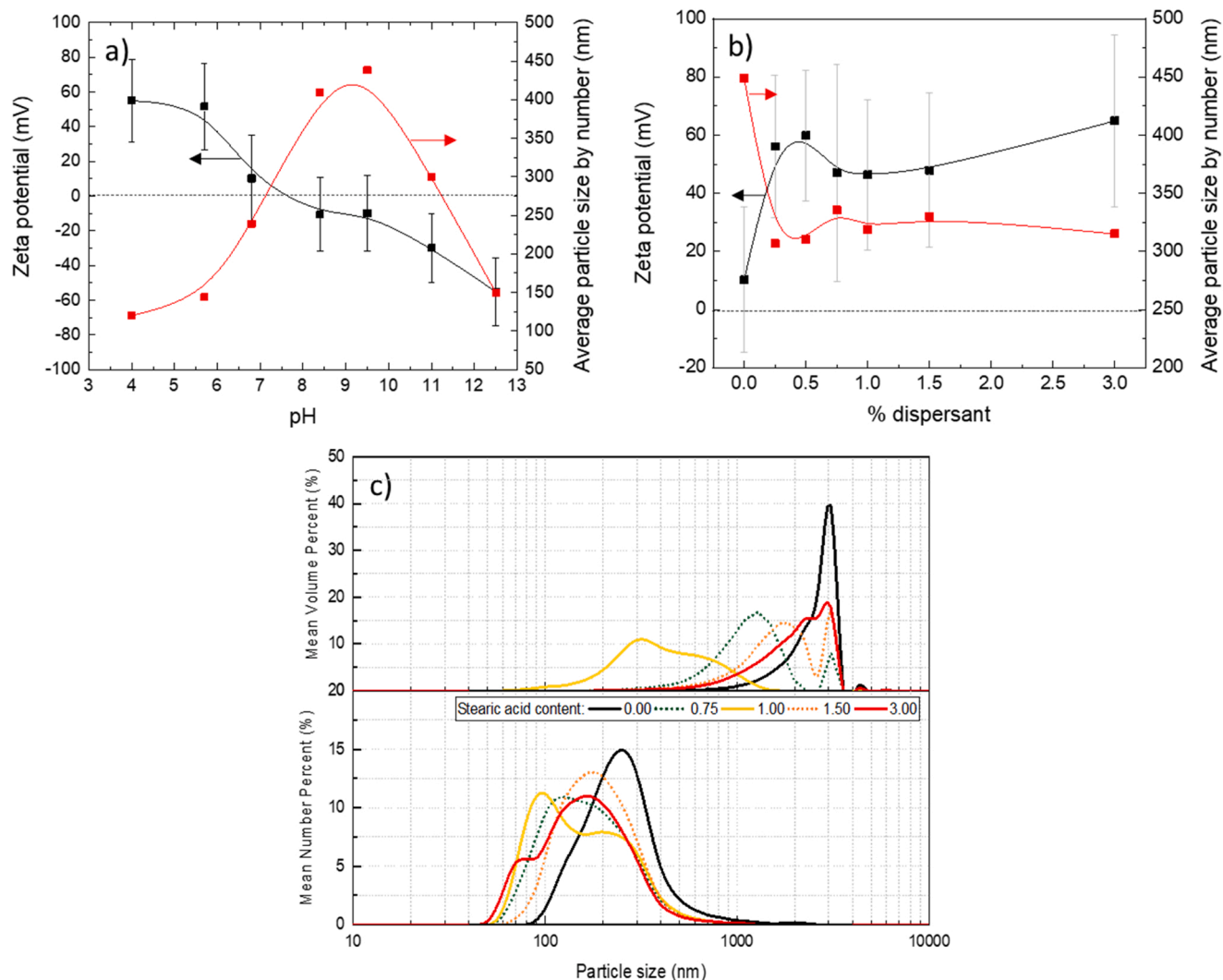
## 2.3. Powder and foam characterization

Synthesized powders were characterized by Differential Scanning Calorimetric (DSC) and Thermal Gravimetric (TG) analysis using a Q20 calorimetry unit (TA Instruments, USA) in air to determine the optimal calcination temperature. The crystallographic phase and oxidation state were determined after calcination with XRD (X-Ray Diffraction; D8 Advance A25, Bruker) and XPS (X-ray Photoelectron Spectroscopy; Phoibos 150 MCD, SPECS) analysis, respectively. The particle morphology, size, and Al distribution were estimated by Transmission Electron Microscopy (TEM) using a TALOS F200S (FEI, USA) microscope.

To establish an optimal dispersant content in camphene media, calcined powders were suspended in EtOH (ethanol) with concentration of 0.1 g·L<sup>-1</sup>, since camphene evaporation could disturb the measurement made using the Zetasizer Nano ZS equipment (Malvern Panalytical, UK). The pH was modified by adding drops of HNO<sub>3</sub> or Tetramethylammonium hydroxide (HTMA) to reach acid or basic values, respectively before power addition. Two pH fixed slurries (pH 6 and 9) were prepared with different content of SA (0–3 wt%). The particle size was also measured. After slurry preparation with camphene, a Tensor II spectrometer (Bruker, UK) was used to acquire the FTIR spectra in transmission mode on samples with different content of SA. About 1.5 mg of the green sample (after camphene sublimation) were diluted with KBr powder (1:100 ratio) to form thin pellets using uniaxial compression. The acquired spectra were collected with a resolution of 8 scan·cm<sup>-1</sup>. Pore size distributions were characterized for powders processed with different amounts of SA, by Mercury Intrusion Porosimetry (MIP) using a Micromeritics AutoPore IV 9510 (USA), and by the N<sub>2</sub> adsorption/desorption isotherms and BET specific surface area with an Accelerated Surface Area & Porosimetry (ASAP) system (Micromeritics ASAP 2020 (USA)).

The sintered Fe3Al foams were characterized by Scanning Electron Microscopy (SEM) performed on a TENE0 microscope (FEI, USA) and an Optical Microscopy (OM) using a Nikon microscope MA100N across the entire heights to determine the pore morphology. The pore size and cell wall width were estimated by Image Analysis (IA) using the non-redundant maximum-sphere-fitted algorithm [34] of the ImageJ software over the OM images. To estimate the average pore diameter at different sample height, 6 OM images covering a total area of 20 mm<sup>2</sup> were used. Total porosity (%) of the sintered foam was determined throughout Archimedes' method by soaking the samples into boiling water for 5 h following a 24 h immersion in hot water.

A TG analysis, using a Discovery (TA Instrument, USA) analyser, was performed to evaluate the isothermal redox performance on subsamples of the sintered Fe3Al foams with 3 wt% of SA. Subsamples of 3x3x3 mm



**Fig. 5.** Effect of the pH (a) and dispersant content (b) on the zeta potential, electric conductivity and average particle size (by number) of the Fe<sub>3</sub>Al calcined powder at pH 6. The particle size distributions (c) calculated by mean number and volume as a function of the SA addition.

x mm x mm in volume were sectioned from the top part of the sintered foams. The isothermal redox performance was obtained after 10 consecutive cycles at 650, 675, and 700 °C using an alumina plate to support the porous subsample. Gas streams of Ar-10 vol% H<sub>2</sub> and N<sub>2</sub>-10 vol% O<sub>2</sub> (using synthetic air as oxygen source) were used in the reduction and oxidation step, respectively. Sintered Fe<sub>3</sub>Al foams were heated at 50 °C·min<sup>-1</sup> under N<sub>2</sub> flow gas, reducing and oxidizing reaction time were both established at 12 min, and a N<sub>2</sub> flow gas was used to purge the TG between reactions for 3 min. Gas flow rate was established at 200 mL·min<sup>-1</sup> and data points were collected at a rate of 12 data·s<sup>-1</sup>. After redox test, foams subsamples were also characterized by Mercury Intrusion Porosimetry (MIP) using a Quantachrome Poremaster 60GT porosimeter and SEM to evaluate changes in the pore structure.

### 3. Results and discussion

#### 3.1. Synthesized powders characterization

Fig. 1 shows the TG and DSC curves of the as-synthesized powder with 3 wt% of Al<sub>2</sub>O<sub>3</sub>, in its initial gel form, (Fig. 1a) and after drying at 110 °C overnight (Fig. 1b), heating and cooling at 10 °C/min. The TG curve of the gel sample showed five major regions of weight loss: (1) up to 149 °C, a 13.1% of weight loss was due to water and nitric acid removal, (2) at 150 °C, the dehydroxylation of the ferric hydroxide

formed goethite ( $\alpha$ -Fe<sup>3+</sup>O(OH)) exothermally (confirmed by the exothermic peak event at the DSC curve) with a weight loss of approximately 27.2%; (3) from 150 to 203 °C, due to the decarboxylation of the organic moiety some mass was lost (13%), the reductant atmosphere created partially reduce the Fe (III) to Fe (II) given the formation of magnetite [35], evidenced by the XRD spectrum of powder treated at 170 °C; (4) from 203–347 °C, another exothermic peak at 283 °C was detected with a weight loss of 17.3% due to the complete decomposition of the ferric citrate and goethite to form maghemite ( $\gamma$ -Fe<sub>2</sub>O<sub>3</sub>); and (5) above 400 °C a weight loss of 4.2% was noticed corresponding to complete decomposition of nitrate group and citrate precursors (under 2%), the exothermic peaks at 416 °C and 468 °C could be attributed to the oxidation of Al-citrate precursor [36] and the final formation of  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> [37], respectively.

The TG and DSC curves of the dried powder clearly showed the influence of the heat treatment due to the modification of the hydroxylation ratio, as most of the OH<sup>-</sup> ions were previously removed before calcination process. Fig. 1b exhibits four regions of weight loss that could be ascribed as: (1) up to 100 °C, some water and nitric acid remained were removed with a 1.5% of weight loss; (2) from 100 to 242 °C, another 1.0% of weight is lost due to the decarboxylation of the organic moiety; (3) from 242 to 390 °C a 3.8% of weight loss was observed with the present of exothermic peaks at 342 °C. This exothermic peak corresponds to the sequential formation of goethite to

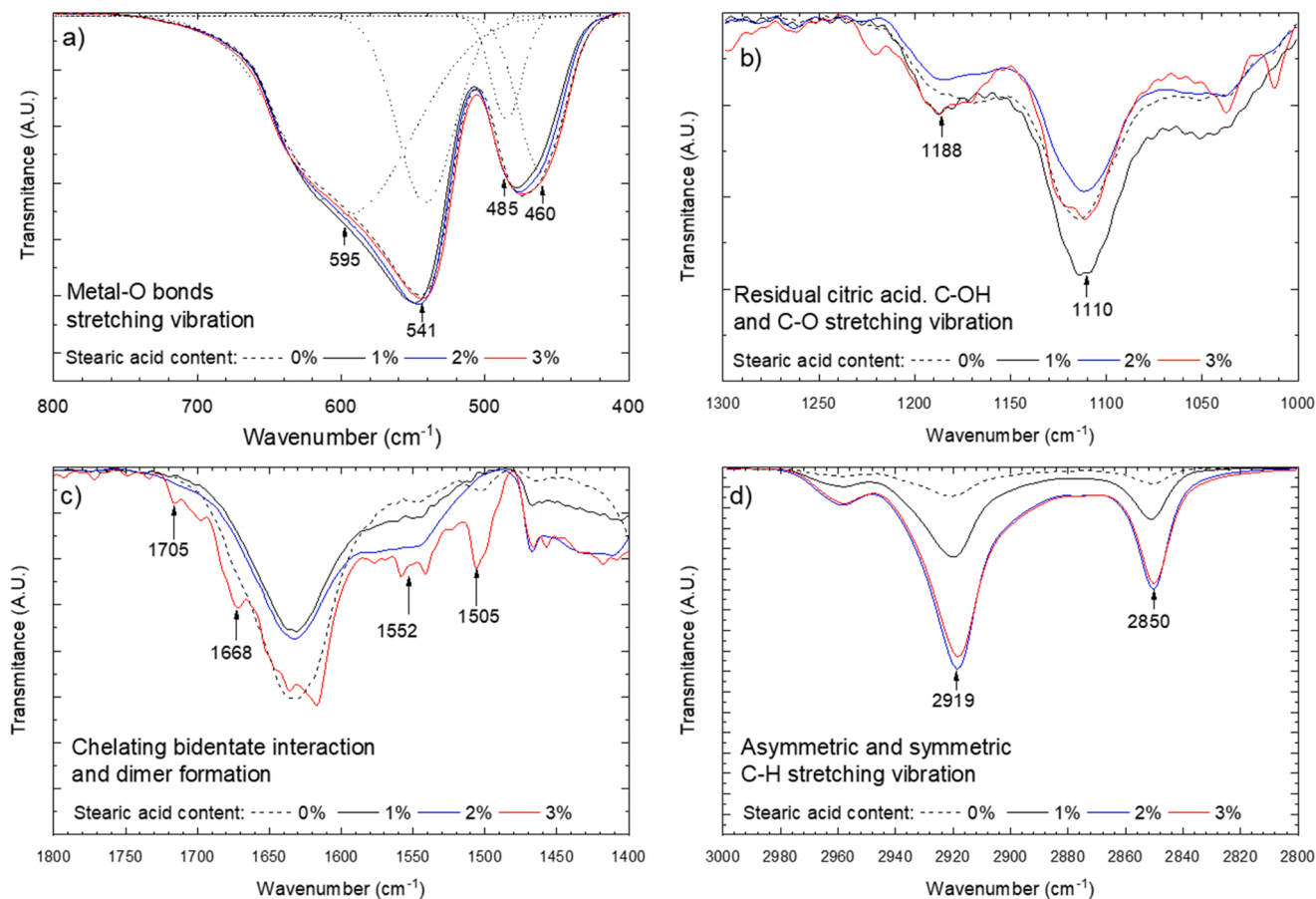


Fig. 6. FTIR spectrums at different wavenumber of Fe3Al calcined powder with different content of SA.

Table 1

Surface area, porosity and pore characterization of the Fe3Al powders with different content of SA based on Mercury intrusion porosimetry (MIP) and by N<sub>2</sub> adsorption/desorption characterization.

Powder feature	Stearic acid content (wt%)		
	1	2	3
BET SSA (m <sup>2</sup> /g)	18.42	16.79	17.32
Open SSA by t-Plot (m <sup>2</sup> /g)	23.09	22.96	23.53
Total pore SSA (m <sup>2</sup> /g)	19.29	18.18	18.79
SSA determined by MIP (m <sup>2</sup> /g)	21.69	23.94	20.17
Total Pore Volume (cm <sup>3</sup> /g)	N <sub>2</sub>	0.12	0.13
	MIP	0.79	0.51
Micropore volume by t-Plot (cm <sup>3</sup> /g)	N <sub>2</sub>	<0.001	0.004
	MIP	664.7	130.4
Average pore (nm)	N <sub>2</sub>	25.61	28.10
	MIP	664.7	280.1
Bulk Density by MIP (g/cm <sup>3</sup> )	0.93	1.12	1.05
Apparent Density by MIP (g/cm <sup>3</sup> )	3.53	2.64	2.72
Porosity (%)	73.76	57.60	60.53

α-Fe<sub>2</sub>O<sub>3</sub> (hematite) [38]; (4) finally above 390 °C, a 1% of weight loss was reported when total citrate precursor with the elimination of residual carbonates occurred at 571 °C [39]. No further transformation was observed beyond 620 °C.

During the TG-DSC characterization, four mayor exothermic events were observed and no mass loss was detected at a given temperature. To corroborated their effects, powder at its gel form were calcined at 170 °C, 350 °C both for 2 h and 620 °C for 6 h, heating and cooling at 10 °C/min, to later perform an XRD characterization (Fig. 2).

XRD patterns in Fig. 2a and b corroborate that the exothermic peaks at 150 and 283 °C of Fig. 1a correspond to the formation of magnetite

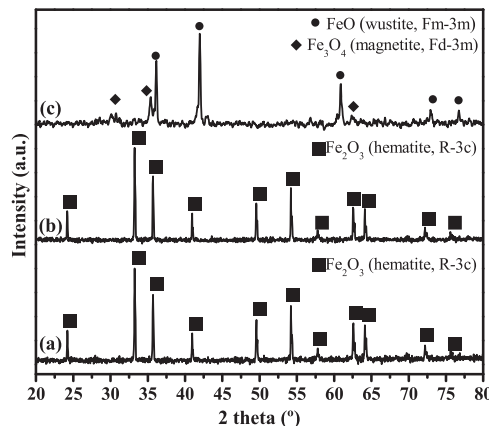
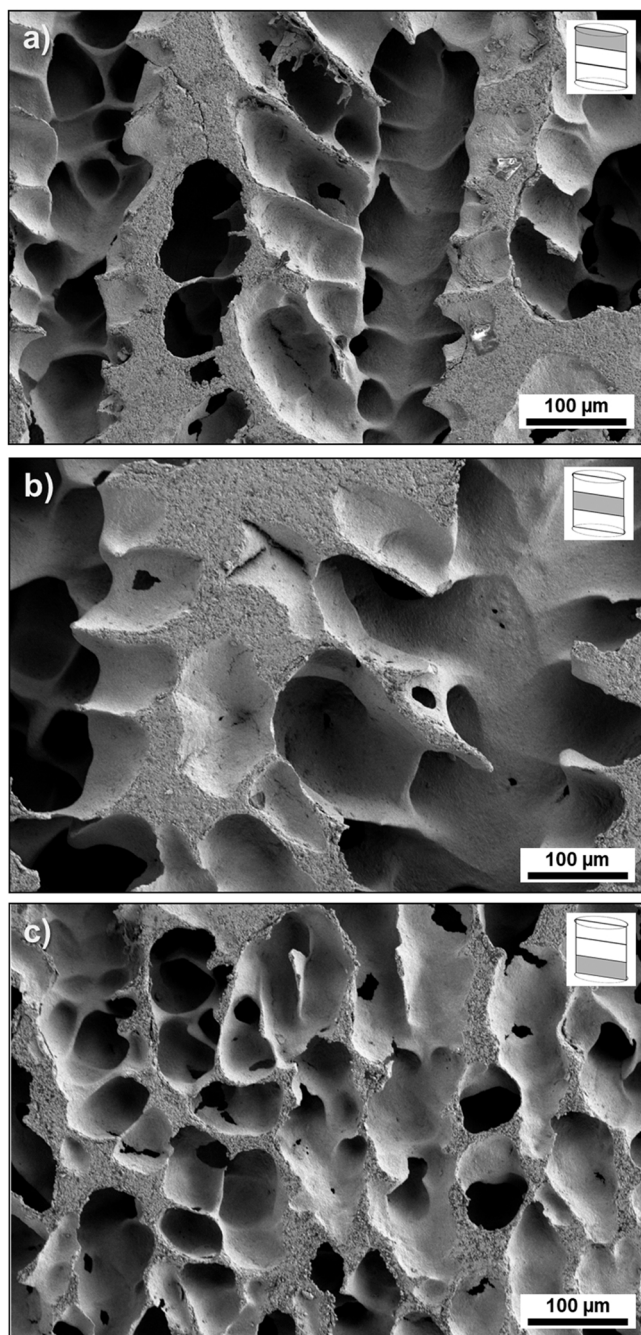


Fig. 7. XRD patterns for the sintered Fe3Al foams fabricated with different content of SA: 1 (a), 2 (b), and 3 wt% (c).

and maghemite (γ-Fe<sub>2</sub>O<sub>3</sub>), respectively. After calcination at 620 °C (Fig. 2c), no Al<sub>2</sub>O<sub>3</sub> phase was initially distinguished due to detection limits and the low calcination temperature [39]. Therefore, the formation of hematite-like solid solution (H<sub>SS</sub>) where Al atoms occupied cationic positions is expected [40–42]. A crystalline domain size of 46 ± 8 nm was calculated for the H<sub>SS</sub> phase using the Scherrer formula for all the diffraction peaks. As can be confirmed by the XRD analysis on the gel and dried powder after calcination at 620 °C for 6 h, both as-synthesized powders generate two pathways of reaction to (eventually) form the H<sub>SS</sub> phase.



**Fig. 8.** SEM images of the sintered Fe<sub>3</sub>Al (with a 3 wt% of SA) foam longitudinal section at different heights: 10 mm (a), 6 mm (b), and 2 mm (c). Micrographs were taken at the axial center plane of the sample. Areas with light contrast represent the solid material.

TEM characterization of the calcined powder at 620 °C showed equiaxial particles with a  $37 \pm 12$  nm in size (Fig. 3a) calculated by image analysis (JMicrovision software), and consistent with the size value determined by XRD. A uniform distribution of Fe atoms and Al atoms colonies scattered at the particle surface (Fig. 3b) is also evidenced. High-resolution XPS spectra (Fig. 4) show the valence state and compositional studies of Fe, Al, and O of the Fe<sub>3</sub>Al and FeOAl synthesized powder. The XPS spectra of Fe 2p of Fe<sub>3</sub>Al powder in Fig. 4a showed two major peaks at 710.9 and 724.2 eV identified with the Fe<sup>3+</sup> ions assigned to Fe 2p<sub>3/2</sub> and Fe 2p<sub>1/2</sub> respectively, and satellite peaks were also identified at 718.6 and 732.6 eV. The major peaks were separated by a spin energy of 13.3 eV, while the associated satellite of

the Fe 2p<sub>3/2</sub> peak was at 7.7 eV, both values were in good agreement with the reported value for α-Fe<sub>2</sub>O<sub>3</sub> in the literature [43,44]. The influence of the Al atoms in hematite solid solution was also visible as the spectra of Fe 2p on the Fe<sub>3</sub>Al powder has moved to slightly higher binding energy (+0.8 eV) as compared with the FeOAl powder (Fig. 4a). The ionic nature of the Al-O bond, in respect to the Fe-O covalent bond, might be responsible for the increased in the binding energy observed in the Fe<sub>3</sub>Al powder. The binding energy of Al<sup>3+</sup> as metal, within a FeAl<sub>2</sub>O<sub>4</sub> phase, and in Al<sub>2</sub>O<sub>3</sub> phase are 73.0 eV, 74.5 eV, and 75.8 eV respectively [45], and the XPS spectrum of Al 2p of Fig. 4b showed a binding energy of 75.4 eV corresponding to cation position in Al<sub>2</sub>O<sub>3</sub> phase in concordance with the TEM observation. The XPS spectrum of O 1s of the Fe<sub>3</sub>Al powder (Fig. 4c) shows a single peak at 530.1 eV (+0.7 eV of the FeOAl powder) broaden to higher binding energies due to the influence of the Al cations, as Al atoms occupy cation position in the H<sub>SS</sub>, the O 1s also moves to higher binding energies respectively [45]. Finally, the synthesized Fe<sub>3</sub>Al powder crystallized as α-Fe<sub>2</sub>O<sub>3</sub> in a hematite-like Al solid solution.

Fig. 5a shows the influence of pH on the zeta potential and average particle size obtained as the mean value determined from the particle size distribution in number of the Fe<sub>3</sub>Al calcined powders. The measurements were made at pH 4 since below pH 3.5 the Poubaux diagram predicts the dissolution of the hematite. The zeta potential of the Fe<sub>3</sub>Al powder moves from 56 to −55 mV for pH values ranging 4–12.5, with an isoelectric point at pH 7.5. The average particle size (estimated by number) shows values of 120 nm and 150 nm at pH 4 and 12.5, respectively. At pH 6 with a zeta potential of 56 mV, the measured particle size was 150 nm, while at pH 7 zeta potential decreases below 20 mV as particle size slightly increases. Therefore, this pH range (6–7) was selected to overview the influence of the dispersant content, since under hydroxyl group of the SA could be slightly deprotonated and negatively charged. Fig. 5b shows the influence of the dispersant content (SA) over the zeta potential and particle size of Fe<sub>3</sub>Al powder suspended in ethanol. As the SA content increases over 0.5 wt%, the zeta potential and the particle size stabilise around 50–60 mV and 300 nm, respectively. It has been reported that SA is anchored to the particle by their carboxylic group [46], favouring the steric repulsion among Fe<sub>3</sub>Al nanoparticles that maintain them dispersed. From 1–3 wt% of SA, although no significant change in the zeta potential and the particle size were detected, most likely due to the maximum Fe<sub>3</sub>Al particle coverage produced by the SA, a slight upturn of the zeta potential can be intuited for a 3 wt%.

The influence of the SA in the stability was explored in detail by comparing the particle size distributions in number and volume (Fig. 5c). The particle size distribution in volume shows a maximum reduction at 1 wt% of SA with a mean value of 330 nm. In fact, with no SA added, the Fe<sub>3</sub>Al particle were poorly dispersed and formed agglomerates of about 3000 nm, but as the SA was incorporated and adsorbed by the particle, their size diminished significantly. Beyond 1 wt% of SA (curves at 1.5 and 3 wt% of SA), Fe<sub>3</sub>Al particles seem to re-aggregate progressively forming groups of particles above the 2 μm. This behavior could be related to an interaction between the adsorbed and dissolved SA molecules acting as binder-bridges that increases the particle size, as have been observed for Fe<sub>3</sub>O<sub>4</sub> coated with oleic acid [47], a similar fatty acid compound. However, these results must be complemented with the particle size distribution in number, as wide size distribution could be deceived due to the low contribution of the smaller particle to the cumulate volume curve. At the size distribution by number, curves showed similar behavior despite the SA content, being the majority of the particles under 400 nm. With SA addition particle size distribution moves to lower sizes until 1 wt%, with a considerable amount of particle below 100 nm then, as the SA content keep rising, distribution curves moves back to higher particle size with no significant number of particles over 1 μm. Therefore, the Fe<sub>3</sub>Al powder with 3 wt% of SA as dispersant agent showed a broad particle size distribution with an average diameter of 150 nm, that is with an agglomeration factor

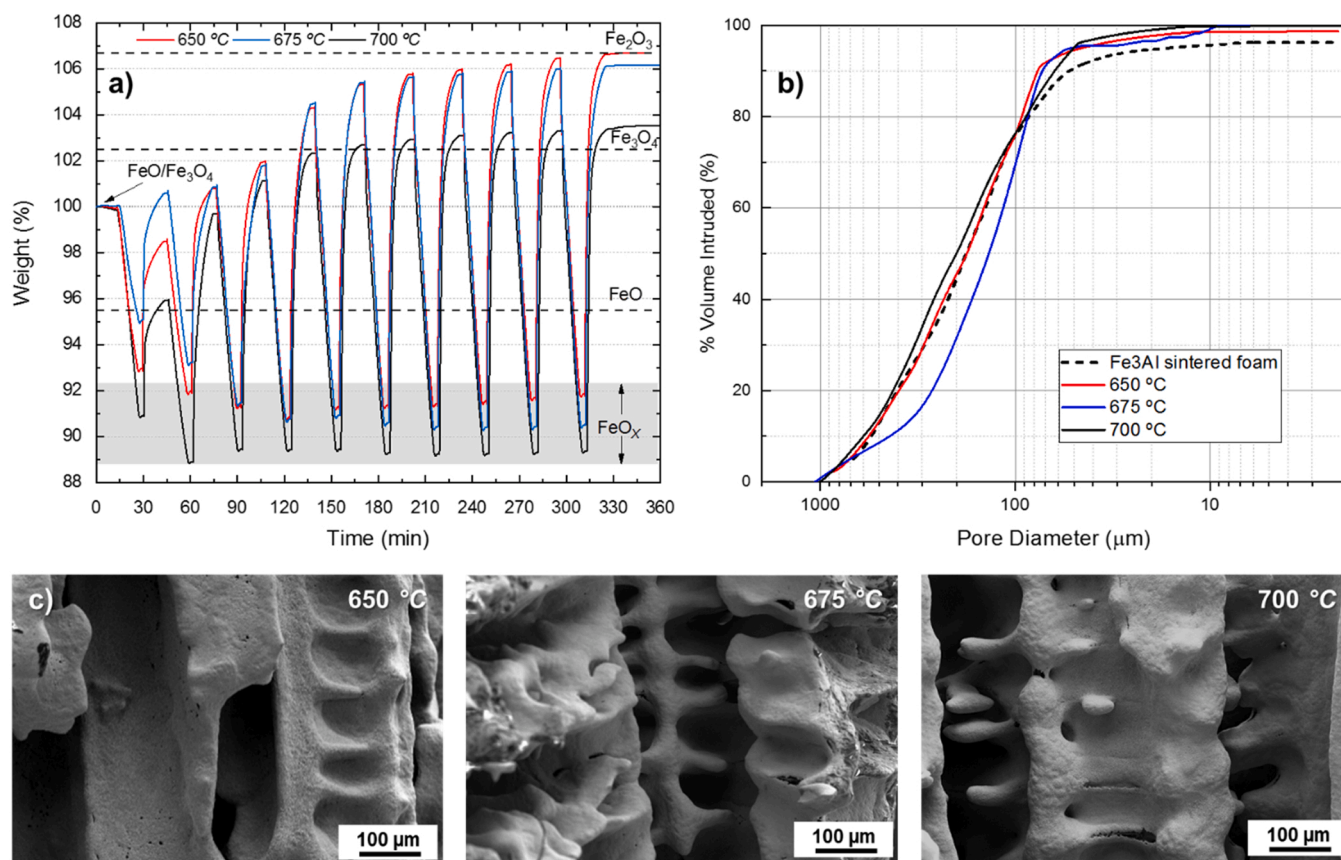


Fig. 9. TG analysis (a), MIP curves of volume intruded percentage (%) versus pore diameter (b), and SEM images (c) at the axial plane of the sintered Fe3Al foams after 10 redox cycles at different temperature (650, 675, and 700 °C). Stoichiometry mass of FeO, Fe<sub>3</sub>O<sub>4</sub>, and Fe<sub>2</sub>O<sub>3</sub> phase (a), and initial volume intruded percentage curve of the sintered Fe3Al foams (b) were included as guideline and comparison in dotted lines.

( $F_{ag} = D_{V50}/D_{TEM}$ ) of 3 since the initial particle size is about 50 nm.

The FTIR spectra of Fe3Al calcined powder at 620 °C further dispersed with 0, 1, 2, and 3 wt% of SA are shown in Fig. 6. Between 800  $cm^{-1}$  and 400  $cm^{-1}$  bands in Fig. 6a, four overlapped peaks (dotted lines) were determined after Gaussian deconvolution due to the oxygen bonds with Fe and Al metal cations in the hematite-like Al solid solution. These peaks were identified at lower wavenumber compared to the literature. Fe-O bonds showed stretching vibrations at 541  $cm^{-1}$  and 460  $cm^{-1}$  [48], while the Al-O bonds showed stretching-vibrational at 595  $cm^{-1}$  and 485  $cm^{-1}$  [49]. Moreover in Fig. 6b, a band attributable to -C-OH stretching appeared at 1110  $cm^{-1}$  and -C-O stretching located at 1188  $cm^{-1}$  due to some residual citric acid [50].

At Fig. 6c, the powders showed a band at 1638–1618  $cm^{-1}$  corresponding to the bending vibrations of the surface hydroxyl group [47]. No peak at 1700–1715  $cm^{-1}$  was determined at 0–2 wt% of SA corresponding to the carboxylic group due to the formation of a single coating layer around the Fe3Al particles bonded by the carboxylic group [47]. However, at 3 wt% of SA the following features were observed: (1) a peak at 1705  $cm^{-1}$  is slightly appeared due to the formation of a multi-layer around the particles [47,51]; (2) the two characteristic peaks at 1668  $cm^{-1}$  and 1552  $cm^{-1}$  belong to the symmetric and asymmetric carboxylate group stretching band,  $\nu_{(COO-)}_{asym}$  and  $\nu_{(COO-)}_{sym}$  respectively, due to the chelating bidentate interaction between carboxylate groups and metal sites [47,52], and (3) the appeared of a new peak at 1505  $cm^{-1}$ . This new peak could be attributed to the SA molecule forming dimers with the free molecule or along coated particles [53] acting as a binder. The absorption peaks at about 2919 and 2850  $cm^{-1}$  in the high-frequency region (Fig. 6d) were attributed to -CH<sub>2</sub>- band asymmetric and symmetric stretching vibrations of SA, respectively. These peaks were more intense as the SA content increased.

The dimers and the chelating interactions might be responsible for the enhancement of green strength observed in the Fe3Al foam with 3 wt % of SA, as they might be acting as a binder agent, since slurries with 1 and 2 wt% of SA were also created to manufacture Fe3Al foams according to Section 2.2, but the samples crumbled after de-moulding and camphene removal. Also, the slurry with 1 wt% of SA showed high viscosity and was difficult to pour into the mould, which could be linked to the significant number of particles under 100 nm observed in Fig. 5c.

Table 1 collects the main morphological properties of the Fe3Al powders with different content of SA from the green sample after been resulting from the porosity exploration. N<sub>2</sub> adsorption/desorption data analysis evidences a wide specific surface area (SSA) of the shaped parts (>10  $m^2/g$ ), with a total absence of microporosity. The BET surface area and open SSA maintains around 17 and 23  $m^2/g$ , respectively, exhibiting lower values for the 2 wt% SA powder. However, the SSA determined by MIP ranges 20–24  $m^2/g$ , having the highest value (23.94  $m^2/g$ ) this of the Fe3Al 2 wt% SA powder.

In all powder samples, the total pore volume is higher for the range of pores determined by MIP (0.51–0.79  $cm^3/g$ ) than for porosity determined by N<sub>2</sub> adsorption/desorption (0.12–1.14  $cm^3/g$ ), and consequently the large mesoporosity has a higher contribution to the porous structure. Main porosity determined by those techniques, N<sub>2</sub> adsorption/desorption and MIP, are in the range of 31–26 nm and 665–130 nm, respectively. Differences in SSA, volume and size of pores suggest qualitative and quantitative differences in the porous microstructures only depending on the particles stabilization/surface modification and/or the binder role of SA. The powder prepared from particles dispersed with 1 wt% of SA, exhibits the highest porosity (73.76%) with pores ranging from 665 nm to 23 nm. The addition of 2 wt% of SA to stabilize the nanoparticles suspension leads to a less porous microstructure

(57.60% of porosity) with the smaller and narrower pore size distribution (130–24 nm), evidencing the role of binder of the amount of SA added in excess. With the addition of 3 wt% of SA, the powder exhibits a relative similar porosity (60.53%) than with 2 wt% of SA, with large pores in both ranges: 280 nm determined by MIP and 30.76 nm determined by N<sub>2</sub> adsorption/desorption, but with higher apparent density by MIP.

The bulk density increases as SA content increases, which is in line with the mechanical stability of foams shaped after the evaporation of the camphene. The Fe3Al powders processed with 3 wt% of SA is the only material maintaining its shape after freezing. The increase of bulk density and mechanical stability is also in line with the decrease in the pore size of powders processed with 2 and 3 wt%. On the other hand, the apparent density can be considered equivalent to the density of the powder skeleton, the density of the material to which mercury does not have access. This density is higher when the nanoparticles are better dispersed (with 1 wt% SA), but the low solids content considered and the high rheology of the suspension will make the material lack physical integrity. Powders processed with 2 and 3 wt% SA have lower apparent densities, and it is the effect of the binder that will allow the foam to maintain its mechanical integrity after drying, with a lower volume and size of pores. Therefore, the combining effects of the higher bulk density, medium porosity and the seemingly binder properties of the SA, could explain the high performance of foams after freezing when using suspensions stabilized with a 3 wt%. Structural stability of Fe3Al foams obtained with 3 wt% of SA makes them optimum to be used to fabricate the sintered foams.

### 3.2. Doped Fe<sub>2</sub>O<sub>3</sub> foam characterization

The XRD analysis performed over the sintered Fe3Al foams prepared with 1, 2 and 3 wt% of SA (Fig. 7) shows significant results. The use of 3 wt% of SA produced a reduction of the Fe<sub>2</sub>O<sub>3</sub> phase to a combination of FeO and Fe<sub>3</sub>O<sub>4</sub> phases, when lower SA content (1 and 2 wt% of SA) did not produce any hematite reduction. According to the literature, the use of up to 3 wt% Al<sub>2</sub>O<sub>3</sub> enhances the reduction process of Fe<sub>3</sub>O<sub>4</sub> due to the formation of a network-like structure of FeO [54,55]. These studies employed a CO-CO<sub>2</sub> gas stream as a reductant source, but here sintering process was performed in a close cylindrical furnace, being the only reductant source, the carbon atoms present in the SA molecules (C<sub>18</sub>H<sub>36</sub>O<sub>2</sub>). Reduction of iron oxide via organic compounds have been reported previously [56]. But, it was not observed in similar research when polystyrene ((C<sub>8</sub>H<sub>8</sub>)<sub>n-1</sub>) and oligomeric polyester (C<sub>90</sub>H<sub>172</sub>O<sub>10</sub>) were used as binder and dispersant agent, respectively [24]. In this case, the reduction process might be enhanced due to the local concentration of organic compound via the covering of the Fe3Al powder by SA molecules and the presence of higher Al<sub>2</sub>O<sub>3</sub> content. Quantitative phase analysis was performed by Rietveld analysis over the sintered Fe3Al foam with 3 wt% of SA where a 77.2 and 22.8 wt% of FeO and Fe<sub>3</sub>O<sub>4</sub> phases were respectively, determined.

As for the foam pore structure, the cooling system employed in this research generates a directional solidification with a non-constant cooling rate where the thermal gradient decreased, and the solidification front velocity increased throughout the sample height [57]. This cooling procedure promotes significant differences in pore morphology along the cooling direction, as it is shown in Fig. 8. The SEM images were taken at the axial central plane of the sintered Fe3Al (with a 3 wt% of SA) foam display a significant branched pore structure at the bottom part, while the rest of the sample shows pores with a well-defined dendritic shape. These different pore structures were promoted by the use of nanometric powder and the variation of the cooling rate throughout the sample height.

At the lower part of the samples (near the mould bottom), the rapid cooling produces the rapid formation of a camphene solidification front. The nucleation and growth of numerous dendritic crystals impinging each other have created an interconnected solid structure that has

pushed the particles to the interdendritic spaces (Fig. 8c). As the solidification front moves within the sample (middle and top part), the reduction of the thermal gradient increases the solidification front velocity leading to elongated camphene dendrites (Fig. 8b) with well-defined secondary arms (Fig. 8a). The average pore diameters, estimated by image analysis, were 170 ± 15, 199 ± 18, and 126 ± 17 μm in areas described by Fig. 8a–c, respectively. The density of the sample was estimated by Archimedes method on 1.24 g·cm<sup>-3</sup> with an open and close porosity of 75.0% and 1.3%, respectively. The use of SA reduced the aggregate size of the synthesized powder dispersed in camphene improving the dendrite contour replication during solidification and increasing the pore size. This improvement is based on the increase of the critical velocity for particle engulfment ( $V_{cr}$ ) proposed by Stefanescu [58] which is roughly  $V_{cr} \approx 1/D$  (being  $D$  the particle diameter), below this velocity particles are pushed rather than trapped by the solidification front. Therefore, camphene crystal could grow by pushing the particles within a much wider range of velocity, also reproducing the dendrite contour much better.

### 3.3. Redox performance of the sintered Fe3Al foam

According to Rietveld of the XRD diffraction in Fig. 7, the sintered Fe3Al foam with 3 wt% of SA presented a 77.2 wt% of FeO and 22.8 wt% of Fe<sub>3</sub>O<sub>4</sub>. Therefore, if complete reduction of the foams were achieved a 74.2% of mass reduction would be obtained. In turn since the oxidation step was performed in air due to experimental limitation, the complete oxidation of Fe would create Fe<sub>2</sub>O<sub>3</sub> with a mass gain of 106.3%. Fig. 9a showed the TG analysis of the sintered Fe3Al foams during 10 isothermal redox cycles. A full reduction was not achieved at any tested temperature due to the duration of the reduction step, instead an over oxidation was recorded due to the use of synthetic air. Foams retained their redox performance during cycling, as they gained weight in all cases, reaching faster a steady-state when operando temperature decreases.

According to the literature [59,60], hematite follows a two-step reduction process where on the first step Fe<sub>2</sub>O<sub>3</sub> reduces to Fe<sub>3</sub>O<sub>4</sub>, at the second step, Fe<sub>3</sub>O<sub>4</sub> is reduced directly to Fe or forms FeO as a transition phase. In this case (Fig. 9a), samples were partially reducing to a FeO<sub>x</sub> phase with  $X$  being approximately 0.79, 0.75, and 0.69 for 650, 675, and 700 °C, respectively. During reoxidation, the use of O<sub>2</sub> promotes the direct formation of Fe<sub>2</sub>O<sub>3</sub> phase, while steam will only promote the generation of Fe<sub>3</sub>O<sub>4</sub> phase due to thermodynamic restriction. Therefore, the mass gained up to stoichiometry mass of Fe<sub>3</sub>O<sub>4</sub> phase will correspond to a hydrogen production if a steam flow had been employed. At 700 °C, TG analysis (Fig. 9a) shows the highest degree of reduction and, at the re-oxidation step, the stoichiometry mass line of the Fe<sub>3</sub>O<sub>4</sub> phase is overpassed at all operando temperatures. These results suggest that Fe3Al foams are able to produce hydrogen with the use of steam with no reduction in redox performance during the redox cycling.

Regarding the pore size and morphology, no significant variation on the cumulated volume intruded curves were observed before and after redox test (Fig. 9b). Pore diameter at 50% of volume intruded were estimated in 160–200 μm for sintered samples before and after redox test, those values are in good correlation with results obtained by image analysis on Section 3.2. Also, the SEM image analysis on Fig. 9c reveals not significant changes as compared by initial pore morphology on Fig. 8a, and dendritic contours are retained after the redox cycles at all temperature. This is especially interesting, as foams recover all the weight during oxidation, gain further more mass until full re-oxidation, and showed no sign of performance reduction or structural degradation.

## 4. Conclusions

Hematite foams have been successfully developed by freeze-casting for redox applications. The synthesis of the nanometric powder by



coprecipitation, and the use of SA as dispersant/binder agent results in the production of foams with pore sizes over 100  $\mu\text{m}$  with enhanced dendritic contour definition. SA has a relevant role structurer, and also acts as a reductant agent over the hematite nanoparticles. Sintered foams were able to withstand 10 redox cycles with adequate performance as no significant effect on the porosity was observed. The comparison of the hydrogen production with the oxidation reaction seems valid and useful, as the gain weight was over the stoichiometry value of the  $\text{Fe}_3\text{O}_4$  with no structural degradation of the foams. Future works will focus in testing a higher number of redox cycles within a wider range of temperature and using steam as oxidizing gas.

### Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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