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SOLUBLE SURFACTANT EFFECTS

ON GAS ABSORPTION OF ORGANIC COMPOUNDS

BY

ANGELO C, MORRESI

A THESIS

PRESENTED IN PARTIAL FULFILLMENT

OF

MASTER OF SCIENCE IN ENVIRONMENTAL ENGINEERING

ΑT

NEWARK COLLEGE OF ENGINEERING

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Newark, New Jersey

1975

APPROVAL OF THESIS

Ву

ANGELO MORRESI

For

DEPARTMENT OF CIVIL & ENVIRONMENTAL ENGINEERING NEWARK COLLEGE OF ENGINEERING

By

FACULTY COMMITTEE

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Approved:

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Newark, New Jersey

May 1975

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ABSTRACT

A literature search dating back to the beginning of this century turned up no previous work similar to ours. We discuss several methods and experiments involving the scrubbing of air streams.

The objective of this work was the determination of surfactant affects on the solubility of certain organic compunds of varying solubility in water. A means of simulating a packed tower was devised to allow for bench scale evaluation and thus enabled a greater number of organic compounds to be examined with a greater variety of surfactants.

Curves were plotted based on organic vapor concentration, surfactant concentration, organic type, surfactant type, and the initial organic in water concentration. Vapor pressure data was determined through use of gas chromatography techniques.

Data was analyzed with respect to surfactant type and considerations were given to surfactant critical micelle concentration and its effects on each organic compound. Trends in solubility differentials as a result of surfactant concentrations were observed and noted.

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INTRODUCTION

The removal of gaseous pollutants from an air stream is mandatory, both for health reasons and law requirements. A gas absorption process, sometimes accompanied by a chemical reaction, is usually used for the removal of noxious gases such as hydrogen, fluoride, hydrogen sulfide, hydrogen chloride, and chlorine from an air stream. This method involves the removal of the contaminant gases from the gas stream into a liquid in which it is soluble or partly soluble. The two basic factors controlling this gas absorption process are (1) the degree of solubility of the gas to be removed in the liquid used for scrubbing, and (2) the means of obtaining intimate contact between the gas and liquid streams to bring about the quickest absorption rate possible. In processes which use gases that are less soluble in the liquid media, caustics or salts are introduced to react chemically with these contaminants. An example of this would be the use of sodium hydroxide as a scrubbing liquid to react with chlorine to produce relatively harmless sodium hypochlorite.

Those organic compounds which are normally immiscible or partly miscible in water can be gas contaminants also and their subsequent removal from a gas stream by a liquid medium is dependent on their solubility in that medium. Water, the most economical liquid scrubbing medium by far, must be examined for possible use. Immiscibility and therefore the solubility of one compound in another is a function of the physical properties 2 of the solute-solvent interface. Bonilla and Baron studied the absorption of ethylene oxide in a packed column with variours aqueous and mon-aqueous solvents. They varied the gas temperature and concentration in the air stream passing through the column and concluded that the liquid-film resistance is the controlling factor for absorption.

Othmer and Scheibel in doing work with acetone in a semicommercial packed tower; varied the range of concentration of acetone in the air and in the washing solutions. They found the rate of acetone absorption by the water was dependent on both the liquid and gas films. Interfacial resistance seems to be the governing factor determining mass transfer and mass transfer rates. Emmert and Pigford found that in falling liquid films, mass transfer rates were greater when rippling occurred as the gas (i.e. they examined CO₂) passed through it rater than when there were The addition of surface active agents elimino ripples. nated the rippling of the liquid. In some part greater transfer rates can be attributed to there being less surface area on a straight sheet than on a liquid sheet with Shou found this to be true in devising a rippling motion. apparatus for absorbing gases and vapors. He immersed a mem-

-2-

ber of great surface area into the liquid and withdrew it, thereby subjecting the gas to be absorbed to a large surface of film of absorbing liquid. Thousands of patents were issued over the years for just the above type of process. The absorption of gases in liquids has inspired many a researcher and some of their works will be discussed.

In discussing the principles of gas absorption Lewis 6 and Whitman tell us that when a liquid and gas come in contact, there are film layers between them. On the gas side as well as the liquid side of the interface there is a film layer in which motion by convection is slight. Therefore, the transfer of solute through the films is by slow diffusion and they are the controlling parameters of absorption. They devised the following equation pertaining to absorption:

Rate of absorption = $\frac{dw}{Ad\Theta}$ = Kg(Pg - Pi) - Ki(Ci - Cl)

w---weight of solute (grams)

 θ ---time (hours)

P---concentration of solute in gas (atmosphere)

g---outside gas film

i---interface

1---inside liquid film

Lewis and Whitman further explain that mixing increases the interfacial area between the gas and liquid and from this standpoint alone absorption increases.

Confirming this work, Donnan and Masson in formulating their theory of gas scrubbing towers with internal packing, have come up with the following criteria for higher absorption efficiency:

- a) The interfacial area between the gas and washing liquid must be large.
- b) There must be a high relative motion between gas and liquid.
- c) There must be a degree of turbulent motion in one or both phases.
- d) There must be a sufficient rate of flooding to obtain the maximum drip effect.

Mixing obviously accomplishes the first three criteria and should increase absorption.

Free turbulence and the diffusional processes developed under its influence was analyzed by Kafarov and 10 Troimov. They studied the absorption of HH₃, SO₂, Me₂CO, EtOH, and CO₂ from air streams by water in a packed tower. The packed volume varied from 0.25 liters to 9.15 liters and the gas rate, G, from 2.3 to 31 cubic meters/ hour and the liquor rate, L, from 5 to 160 liters/hour.

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They also varied packing types, thus free space of the tower. From their data they found that only turbulent mass transfer is controlling when diffusion is concerned.

However, as was seen previously, absorption is controlled by the physical properties of the media involved, and in order to have an absorption rate to influence, one must first have absorption. V. Koran studied the action of vapors of some organic liquids on the surface tension of water. Saturated vapors of CCl₄, C₆H₆, PlMe, benzine, CHCl₃, Et₃N, and Et₂O were passed through water and the surface tension was measured. The surface tension varied over the range or organics used, but it was found that the surface activity of these vapors and their effect on water parallel the interfacial activity of the corresponding organic liquid phases upon water.

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Schwartz and Perry explain that most organic compounds which are soluble in water lower its surface tension, however a brief explanation of surface tension seems necessary.

Van der waal's forces occur between one molecule and another in a liquid. For the molecule surrounded by other molecules, i.e. one at the liquid interior, the resultant force is zero, however, the molecule at the liquid surface is subjected only to forces which tend to pull it inward. The liquid, as a result, takes the form with the

-5-

least surface area per unit volume. Thus we note drops are spherical. This tendency for contraction and the forces associated with it is considered free energy, and this free energy per unit area is called the surface tension.

E. Filippi did some work with other absorption in certain liquids. He measured the surface tension of various colloidal solutions. Emulsions formed when the differences in surface tensions of the two compounds was not very large. Emulsions did not form when surface tensions were large. Emulsions are the dispersion of one liquid in another liquid, the two being immiscible or partly miscible. Obviously absorption of a gas from a stream of air is dependent on the properties of the surfaces of gases and liquids that come in contact.

Dubinin discusses absorption as a function of surface layers of absorbent and absorbate. During the time the gas first comes in contact with the scrubbing liquid and it is detectable in the liquid, the absorbent may be divided into three regions: (1) a layer next to the entering surface saturated with gas, (2) an operating layer in which gas is being absorbed, (3) a layer not yet reached by the gas. As the above layers form or fail to form, absorption is effected and their formation is affected by gas velocity, cross sectional area of scrubbing device, maximum concentration of absorbed gas per unit volume of absorbent, vapor

-6-

pressure of the gas. Brown's fundamental principle governing the process of gas washing for the recovery or removal of a gas or vapor component is that the scrubbing liquid can absorb the gas or vapor until the vapor pressure of the latter in solution is equal to the partial pressure of the gas or vapor in the gases entering the washing unit.

13

Summarizing the previous work cited on absorption, and our main interest in absorption of gases in packed 14 towers, we find that Baker has defined the absorption of a gas from a gas mixture by a liquid in a packed tower as a product of five factors:

- The theoretical absorption--- the vapor pressur^e of a gas in a liquid phase equals the partial pressure of the gas in the gaseous phase. The liquid will be saturated with gas when the absorbed gas exerts no pressure.
- 2) The difference in these partial and vapor pressures---This difference is the force which determines rate of absorption and will not equal zero in commercial work.
- 3) The intimacy of contact of gas and liquid phases.

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- 4) Contact time of gas and liquid phases.
- 5) A proportionality constant that depends on the units in which the other factors are expressed.

Our main com ern, however, is the removal of specific cases, namely organic vapors, from a gas mixture or air stream. Several methods have been investigated and the following are included:

- 1) Carbon adsorption of the organic vapor.
- 2) Atmospheric combustion of the organic vapor.
- 3) Catalytic combusion of the organic vapor.
- 4) Condensation of the organic vapor by cooling the gas stream.

Original Methods of Gas Stream Scrubbing

Literally thousands upon thousands of patents and papers have been issued and presented on the subject of gas removal from a gas mixture by a scrubbing liquid. Before discussing some of the methods for organic vapor removal from a gas stream, we will discuss some of the early methods and apparatus for gas in liquid removal.

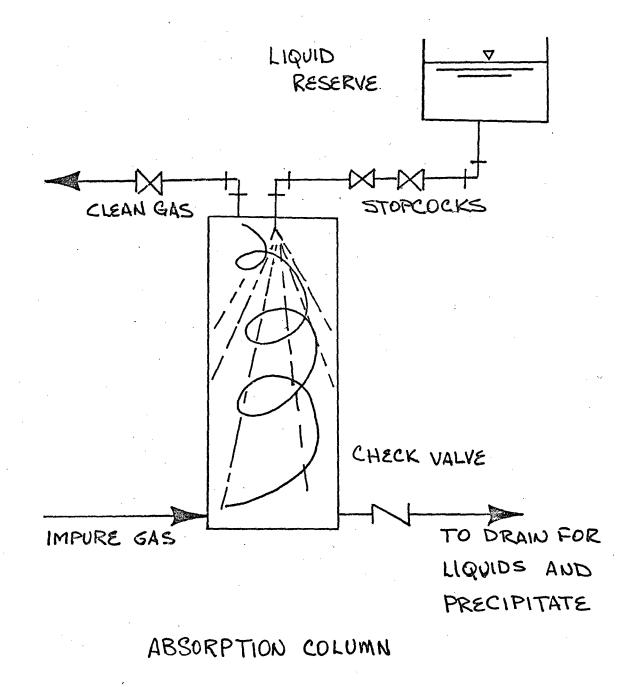
S. Kohn back in 1907 wrote of a more efficient means of utilizing absorption towers. He passed a dilute gas through a series of absorbing towers under uniform con-

-8-

ditions and calculated the amount of gas unabsorbed. The quantity of gas absorbed in proportion to the total quantity of gas passing through the tower was defined as P/Q, and by solving simultaneous equations he found the gas lost to average around 8.3% for all towers. P/Q varies with tower size, water quantity, and manner of distribution, and rate describes an absorption column to be of gas flow. Billv for continuous use and he concurred that using them in series removed a high percentage of impurities. Using absorption towers in series effects the removal of two or more impurities with two or more liquids. Billy's column permitted the purification of any gas by absorption of impurities in any liquid necessary. A long tube 40 mm in diameter is packed with glass, porcelain, and pumice for a large surface area for the liquid to wet, and because these substances are not readily corrosive. Figure 1 shows a schematic of the column.

Over the years different packings for towers have been devised. Probably the earliest packing consisted of 17 bricks, tiles, earthenware, terra cotta, etc. .. arranged so liquid from one layer drips onto the next layer, thus splitting the liquid drop further and exposing more surface area. Rashig later invented a packing for absorption or reaction towers consisting of small cylinders irregularly 18 arranged. They are dropped in the tower at random. How-

-9-





ever, the latest packing entities are Tellerettes, which have the greatest surface area per unit volume along with a lower pressure drop as the gas passes over them. They also have thousands more interstitial holdup points where the gas is absorbed more readily.

Another type of apparatus allows a tower to be divided into chambers provided with two or more spraying devices mounted upon separate drive shafts. The gas to be cleansed rises through the sprays of liquid discharged by One could write a book on all the centrifugal action. different processes devised, such as a horizontal cylinder with rotating disks mounted axially in the liquid chamber. Gases pass across the disks that are wetted and absorb impurities. Disks are coated with earthenware, enamel, cement, 20 or asbestos for protection. Other columns used plates superactivated charcoal, silica gel. imposed upon one another, Other methods include the bringing of vapors of volatile li-23 quids into contact with cold walls and causing condensation, and the idea of bubbling the impure gas through the absorbing liquid by having the bubbles follow the path of a spiral-24 ing tube through the liquid.

Methods of Organic Vapor Removal

Our concern is with the removal of organic vapors from an air stream and because of activated carbon's affinity for organics, its use in water and air pollution is widespread. However its use is limited in low concentrations and because of the necessity for constant regeneration and high initial costs, installations are held down. Some of the 25 earlier applications will be discussed. R. Kattwinkel used a metal cylincer 410x65 mm with 100 grams of activated carbon packing. A measured amount of gases with organic vapors, such as benzine or benzene, were introduced to the cylinder and the benzine or benzene was adsorbed by the activated carbon. The organic vapors were recovered in a condenser and then a receiver when steam at 300°F was passed through the 26 cylinder to drive out the adsorbed gases. Berl and Andreas did similar work with activated carbon. They recovered vapors of organic materials from mixtures of air and water vapor on the carbon. Vapors of organic compounds, such as Et20, MeOH ErOH, C6H6, CC14, acetone with high molecular weights and high boiling points can be recovered, and it was noted that repeated use of carbon reduced its efficiency.

One of the earliest patents issued for separating organic vapors was to Bayer & Co. in 1916. The found the separation of organic gases or vaporized organic substances from their mixtures with air or other not absorbable gases, such as hydrogen, is effected by treatment of the mixtures

-12-

with porous carbon. The extraction of the organic substances 27,28 28 28 from the carbon was with steam. Englehardt adsorbed ether from an air stream on activated charcoal. 1 kg. of highly activated charcoal may adsorb as much as 200 gms of 29 ether. Further work was done in the area of Kattwinkel, and Esons and Wheaton, until the present where highly sophisticated control systems, regeneration methods, and chemical extraction processes are applied, but the simplicity of activated carbon remains the same.

Absorption of organic gases has been effected on 31 32 29 rubber and rubberized fabric, tar oils, silica gel, 33,34 35,36,37,38 etc. Apparatus and methods for their removal and recovery become redundant.

Many of the methods cited and available are not practical on the commercial scale and those that are applicable, are possible only with a relatively high capital investment and/ or a high operating cost.

Absorption of Organic Compounds

It is generally considered impractical to collect water immiscible organic compounds from the vapor phase in water with a high degree of efficiency. One of the principal reasons has been the organic compound vapor pressure or partial pressure contribution to the gas phase of the system once equilibrium has been reached. This partial pressure at equi-

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librium conditions reduces the driving force of collection by water, restricting it to a condensation rather than one of adsorption. Condensation is limited because packed tower operation is usually carried out at elevated or at best ambient conditions. Water scrubbing of organic vapors is limited, however some of the previous works on the subject will be discussed.

38 Sunkov, Kuznetsova and Gorinov followed the absorption of phenol vapors from waste gases in a water scrub-The absorber was 1: 1 meter diameter by 2.2 meters ber. high with perforated plates for a free space of 16.7%. Gas flow was 6000 meters 3/hour which contained 1 gram phenol/ gas and the water rate in the absorber was 1-1.5 meters meters /meters -hour. They did not draw any serious conclu-However the absorption of acetone by water in a sieve sions. plate absorber was investigated by Drozdov, Kisarova, and Sidel' nikova. Acetate concentration in the gas stream was 101.1 mg/l and the liquid to gas volume was 2.36 liters/meters . The coefficient of absorption increased from 2940 to 22,700 (kg-mole/hr)/ (m kg-mole/kg-mole) as the gas velocity increases from .2 to 2 meters/sec. During this same period the efficiency dropped from 93% to 63% thus leaving one to suspect that the absorption is dependent on the time the gas and liquid are in contact, or possibly the size of the sieve plate which

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would allow more gas to comein contact with more liquid. 40 This is what Garbarenko and Stabmikov confirmed as they calculated absorption coefficients of packed columns for absorbing alcohol vapors by water scrubbing. The absorption coefficient was determined experimentally in a packed tower for different velocities of the EtOH-air phase and different flooding velocities of water used for scrubbing. The coefficient was dependent on the gas and water velocities as well as the column dimensions.

Gas film coefficients of methanol, ethanol, and acetone, when absorbed by water from an air stream, were comlul puted. Houston and Walker examined the influence of molecular diffusivity on gas film coefficients in a 12 inch diameter column packed 2 feet deep with linch carbon Raschig rings. Gas rates varied from 100 to 600 lb/hr-ft and water 2 rates from 500 to 2000 lb/hr-ft and it was found that the gas film coefficients were proportional to 2/3 of the gas phase diffusivity.

Absorption of acetylene by water from a gas mixture of 20% acetylene and 80% hydrogen was studied and the packed tower's, packed with Raschig rings, absorbability coefficient 42 was obtained. Sanka concluded that absorption was a case of interphase transfer with the liquid film controlling the mass 43 transfer. This seems to be verified by Konochuk and Stabinkov

-15-

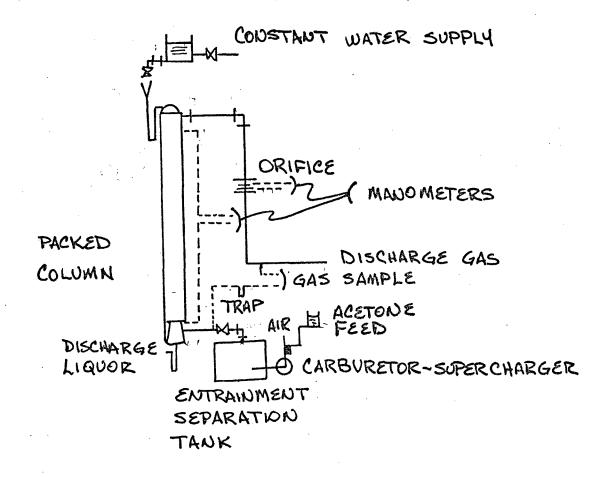
who experimented with alcohol vapors being absorbed by water. They used columns with parallel or zig-zag packing angles of 120° or 90° . Mass transfer increased with decreasing zigzag angle and the zig-zag angle of 90° had the highest efficiency. At the smaller angles the liquid film is broken up to a greater extent as the interstitial hold up points increase allowing greater surface area to be available to the vapors.

This attraction to use water, by researchers, is with good reason, water is plentiful and cheap---the cheapest form of any scrubbing liquid available---therefore when it comes down to applying laboratory work to field installations, the costs versus practicallity curve is brought out and the 100% efficient system is discarded for the most practical system.

44

Othmer and Scheibel used water to absorb acetone from an air stream flowing through a semi-commercial packed tower. Figure 2 shows a schematic of the equipment assembly. The column was 9-7/8" internal diameter, 10" I.P.S., and 19' overall height. The packing consisted of Stoneware Raschig rings that had 1" diameter, 1" length with 1/8" walls. There were 1350 pieces per cubic foot, 73% free space, 58 2 ft exposed area per cubic foot and 80 ft absorption surface per cubic foot of free gas space for a total of $195\frac{1}{2}$ " packing. City water was used for scrubbing and the flow

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ACETONE ABSORPTION BY WATER

FIGURE 2

rate was less than 85 gallons of water per hour per square foot of column cross section. Gas velocities through the column were varied from .6 to 1.8 feet per second and gas concentrations used 1 to 4% of the air stream by volume.

The pressure drop across the column varied with the gas rate. The pressure differential was directly proportion-2 al to increased gas flow. At a gas flow of 481 lbs. air/ft / hr. P was .1236 while at a gas rate of 86 lbs. air/ft /hr. and P=.0058 in. H20 foot/packing. The pressure drop seemed unaffected by liquid flow rate. Recovery efficiency of acetone from the air stream was mostly in the 90-99% range with one down to 60%. However, efficiency over a given set of conditions is a function of column length: the pressure differential, and the gas pumping costs depend on this differential. Therefore the efficiency of acetone removal is dependent on allowable costs for operating the gas fan.

Othmer and Scheibell found the overall gas absorption coefficient KgA to vary with the liquor rate, L, and the gas rate, G, by the following equation.

$$KgA = 1$$

23 + 30
L·⁹⁵ $g^{0.8}$

And since heat affected the above equation, the mass transfer

-18-

also depends on the rate the water could be cooled as a result of a heat exchanger. Acetone condensation would cause the water to heat. Thus many factors must be considered when scrubbing a gas with a liquid, and these factors vary with the gas to be absorbed.

Other organics such as ethanol and ethyl acetate are 45 not so easily removed. In fact laboratory tests have concluded that water scrubbing of air streams containing ethanol and ethyl acetate in a 1:2 weight ratio and in total concen-3 trations from 0.01 lb./Mft to 1 lb./Mft is impractical. Ethanol and ethyl acetate aqueous solutions were prepared containing the desired percent of each by weight. Twenty ml of each solution were placed in flasks which has a head space of 39 ml after they were closed with a rubber serum cap. After standing 18 hours at room temperature (22⁰), one ml of laboratory air was injected into each flask, immediately withdrawn and injected into a gas chromatograph. A Perkin-Elmer 900 Gas Chromatograph, equipped with flame ionization detectors, was used with nitrogen gas as the carrier.

The laboratory tells us the model developed has both mathematical and physical validity, that it describes conditions at equilibrium accurately for the stated temperature. It also explains that the scrubbing out of solvent vapors from an air stream depends on the equilibrium concentrations of the solvent in the gases and the liquid phase.

-19-

Their results showed the minimum amount of water required to reduce by 90% the concentration of ethanol in a 1000 cft air stream was 7.7 gallons, while 288 gallons of water was necessary to reduce the ethyl acetate concentration by 90%. This latter figure is absolutely impractical from the standpoint of equipment size and operational costs. The laboratory also points out that recycling the water to increase the solvent concentration in it and thus reducing costs to make recovery by distillation possible, would not be feasible; because of concentrations in the liquid being too high, not enough or no scrubbing of the air would take place. They also feel further work along the water scrubbing design concept is not warranted and support this with their results.

The scrubbing of organic insoluble vapors in water seems impractical. Further work in the area was done by $\frac{16}{16}$ Cutting and Jones , who studied the effect on the surface tension of water of various vapor pressures up to saturation of benzene, toluene, p-xylene, n-C₅H₁₂, and other immiscible organics. They found that in all cases at low vapor pressures the surface tension decreases almost linearly with increasing vapor pressure, whereas at higher vapor pressures the change in surface tension with respect to the change in vapor pressure increases continuously with pressure. We therefore realize the surface tension of water

-20-

can be affected by organics to some extent to allow for greater absorption, however the adsorbed films are in the gaseous state even when multilayers are formed. And although the life of the adsorbed molecule on the bare surfaceor in a mono-layer or multilayer may be affected by interaction with other adsorbate molecules, they eventually escape back to the gas stream they were traveling in.

Therefore we must change the physical properties of the water by some greater degree that would allow the organics' vapors to be absorbed by the water composition. Surface active agents change the properties of water. They are organic compounds, and like most organic compounds which are soluble in water as we have stated previously, lower its surface tension, and surface active agents do this to 9 the extreme.

A liquid by its tendency towards contraction is actually striving to a state of equilibrium. The function of a surface active agent is to alter this equilibrium sta-47 tus; and its ability to alter the equilibrium state for the desired effect is the basis of a good surfactant.

In a solution of two liquids, the Van der waal's as well as other attractive forces are not equal for each molecule of solute and solvent. The attractive forces of the solvent will be greater than those of the solute, thus the solvent molecules will be pulled away from the surface

-21-

faster than the solute molecules. Therefore there is a concentration of solute molecules with weaker attractive forces at the surface, resulting in the lowering of the free energy, i.e. the surface tension.

The concentration at the phase boundary of one com-9 ponent of a solution is called adsorption. Surface active agents exhibit the tendency to be adsorbed at the phase boundary. The surface active agent molecule is composed of one or more groups which show an affinity for the substance they are dissolved in, called hydrophilic groups; and one or more groups which tend to be expelled by the substance, called hydrophobic groups. Surfactant molecules adsorbed at the water surface will have a majority of their hydrophilic groups towards the aqueous phase and a majority 47 of the hydrophobic groups turned away from the water.

Figure 3 shows a plot of a common surfactant (sodium lauryl sulfate) concentration versus several physical properties as a result of micelle formation. A micelle, or group of molecules and/or ions form at the solution interior. Since there is no surface for adsorption to occur and the hydrophobic and water molecules do exhibit repulsive actions to one another, an aggregate of molecules forms. The hydrophobic links of the surfactant molecule are at the center, while the outside of the micelle is hydrophilic links. Figure 3 notes the sharp changes in solution properties as

-22-

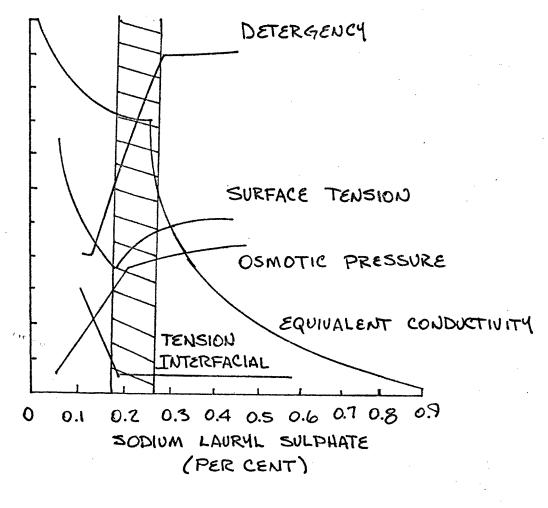


FIGURE 3

the range in concentration of surfactant varies. The surface tension decreases sharply at low concentrations for surfactant and as the cmc range (critical micelle concentration---concentration where large numbers of micelles form) is approached, a sharp increase occurs and then a leveling off because of increased concentrations. As a result of these phenomena, surface active agents can affect the physical properties of water greatly, and thus the absorption properties.

Early work done in this area was by H. L. Barthelemy whose patent mamed the adding of substances such as AmOH, saponin, egg albumin, and preferably the addition of soaps ---K stearate, NH4 oleate---to the scrubbing water to effect absorption of æctone. The acetone is distributed in the form of a foam in the absorption column and scrubbing may take place continuously.

止9

J. R. Pound studied the interstitial tensions between organic liquids and water, and took measurements of the surface tension and of the diffusion of the mutually saturated liquid layers at 30° C. Impurities lessen the tension as a function of time and depending on whether the impurity is an acid or alkali the time period varies. Impurities such as reactive solutes added to water increase the absorption of insoluble or partly soluble gases. Nash recommends this method for the transport of toxic gases across the air-water interface.

-24-

_48

Very early in the twentieth century it was found that in manufacturing emulsifiable solutions of organic substances, the property of suloricinate and alkali so soaps to dissolve certain organic compounds was increased by using a castor oil soap (the castor oil soap was later changed to an 51 alkali sulfide). The castor oil effected the sulorianate's physical properties enough to cause the rise in dissolving power.

52 Dobry-Duclaux investigated the lytopic series Α. These salts increased and decreased the solubility of salts. of organic compounds in water. Salts that increase aqueous solubility, lower the vapor pressure of the water-organic com-Those that decrease the aqueous solubility, pound system. raise the vapor pressure of the system. The salts had their greatest effection volatile organic compounds and decreased in the order as follows: acetone, esters, alcs., nitriles, ethers, saturated and chlorinated hydrocarbons -- where the salts had negligible effects on the latter three. The salts were arrayed in series with each organic compound and the measure of lyotropic behavior was obtained. $ZnCl_2Be(ClO_{11})_2$, Cd(TiBr_L)₂ had the strongest solubilizing action.

The solubility of difficulty soluble compounds to obtain aqueous solutions of organic compounds is further 53 confirmed by I. G. Farbenind. He was issued a French

-25-

patent for his work in this field. Aqueous solutions of phenylethylbarbitaric acid, cyclohexenyl-ethylbarbituric acid, or camphor can be obtained by adding monoalkylamides of lower fatty acids to water and through the use of methylacetamide as an intermediary solvent. Similar work was done by the addition of a hydrogenate phenolic compound such as hexahydrophenol or hexahydrocresol to the absorbing 54 liquid to remove vapors from gaseous mixtures.

Surface active agents therefore /work to allow or increase absorption. The decrease, minimization and subsequent increase in the rate of mass transfer through the liquid gas interfaces with increasing bulk concentrations of surface active agents can be attributed to hydrodynamic changes in the layers adjacent to the interface. The mobility of the interface is determined by the tangential forces which arise from the surface tension gradient, and by the properties of the adsorbed film of the surface active 55agent itself.

56,57Mirev, Elenkov, and Balarev have done much work with absorption and surfactants. The surfactants they worked with were Nekal VKh and OP-10, and it was found in one series of experiments in horizontal columns that they did not affect the rate of absorption of C_2H_2 in water. In the same series of experiments in verticle columns, with the same two compounds, a minimum occurs in the curve of surface

-26-

active agent concentration versus rate of absorption. Thus we find there is a point where adding more surfactant actually hinders absorption. The depth of this minimum varies with the thickness of the liquid, making the column packing an important factor to absorption. It is the packing which disperses the water drops across their surface area.

In subsequent studies the preceding is confirmed--similar work and compounds showed that the hydrodynamics of absorption affect the character of the minimum of the stated curve. As the liquid velocity increases and exceeds a certsin value the minimum disappears because there is greater liquid surface area for the gases to be absorbed. The horizontal column in these studies showed a minimum for the rate of absorption for the gases to be absorbed. The horizontal column in these studies showed a minimum for the rate of absorption to be sharper than other columns and shifted towards the lower concentration of surface active substances. The authors attribute the rate of absorption to the chemical structure of the surface active substances and to the hydro-dynamic conditions of absorption.

Elenkov and Bozhov varied the concentrations of two surfactants---Nekal BX and OP-10 in distilled water. Absorption rates of C_{2H_2} , CO, & CO₂ were determined as a function of stirring. The surfactants increased the absorption rates, but at a high level of agitation, the surfactant

-27-

has no effect. This is due to a removal of the surfactant from the surface of the water to its interior as agitation increases. Thus the hydrodynamics of the water flow is almost as important as the surface active agent.

Further proof of this is stated by Elenkov and Boz-59 hov where the absorption rate of C2H2 in water depends not on the rate of C2H2flow, but entirely on the absorption rate of the water, which can be affected by such things as stirring and/or surface active agents.

A study of the effects of soluble surfactants on 60 gas absorption using liquid laminar jets. The liquid laminar jet was used as the gas absorption contactor since it offers the major advantage of being able to measure interfacial resistances at short contact times when the resistances of the bulk of the liquid phase is very small in comparison. Four soluble surfactants were chosen for study. Dodecyltrimethylammonium chloride, hexadecyltrimethylammonium chloride, dodecyl sodium sulfate and hexadecyl sodium sulfate. A schematic diagram is shown in figure 4 of the laminar jet apparatus.

Pure CO₂ was absorbed into deionized water at different jet rates and with different surfactants present in the water. It was found that the interfacial resistance to gas absorption increased with increasing hydrophobic chain and for a given hydrophobic chain length, the resistance was

-28-

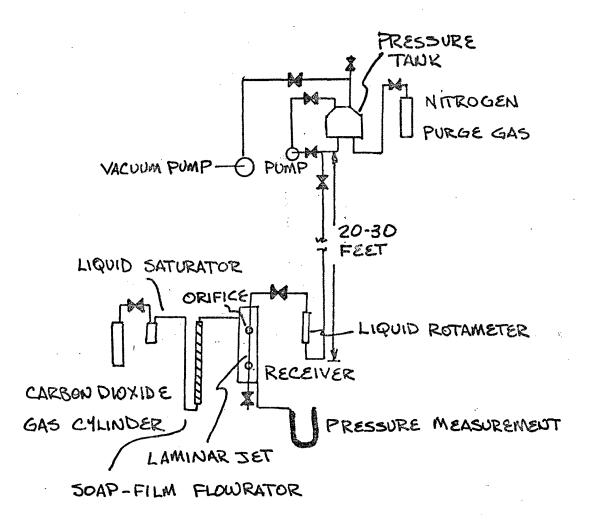


FIGURE 4

higher for the surfactant with the lower molecular mass of the hydrophilic portion of the molecule.

From this previous work we must conclude that immiscible organic compounds can be recovered from an air stream by the use of surfactants or wetting agents modifying the solubility and other variables of the water towards these compounds.

DISCUSSION OF RESULTS

The scrubbing of organics normally considered immiscible or partly miscible from an air stream was considered. The scrubbing liquid was water with small concentrations of surfactant. The investigation followed similar experimental techniques where the investigators determined the scrubbing of ethanol and ethyl acetate with water to be impractical. The introduction of a surfactant to the water has extreme effects on the properties of the water and our experiments try to prove these effects beneficial to increasing the solubility of certain organics in water.

In our experiment we used 50 ml erlenmeyer flasks with rubber serum caps. Various concentrations of water, organic compound, and surfactant were added to the flasks. The water quantity was either 19 ml or 19.5 ml and was added to lml or 0.5 ml of organic compound, respectively. Thus a total of 20 ml of the organic compound-water system filled the flask with approximately 40 ml of headspace. After the addition of from 0.5 to 4.0 grams of surfactant, the rubber serum cap was fitted into place and the solutions were shakened vigorously and allowed to stand and reach the equilibrium state. To reach this equilibrium state each

-31-

flask stood at room temperature (24°C) for 24 hours or more.

A sample of the vapor in the flask (i.e. the headspace) was taken by syringe and immediately injected into a gas chromatograph to determine the organic compound concentration in the vapor. Sample size was in the magnitude of 5.0 ml or 10.0 ml, depending on the organic compound's reaction with the gas chromatograph.

The gas chromatograph used was a Beckman/GC-2 model with a general purpose silicone packing. The following are the conditions set on the gas chromatograph and held constant throughout our tests:

Bridge current---200ma

Gas flowrate---63.4 ml/min

Column temperature---160°C

Recorder chart speed---1/2 inch/min

Chart span---1.0 mv

Room temperature---24°C

Gas type---Helium

Attenuator---setting depended on organic compound's individual reaction with the gas chromatograph and the sample size. For each organic compound tested, the sample size coupled with the attentuator setting which provided the optimum results was used.

Sample size --- see attentuator

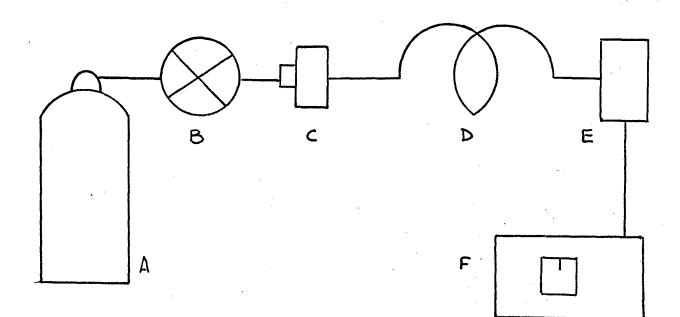
Retention time --- see individual organic charts in appendix.

Figures 5 and 6 are schematic diagrams of the gas chromatograph and the gas flow system. The gas chromatograph was calibrated with 1 ul of liquid organic compound.

Each solution was made in triplicate to avoid gross experimental error; an obviously erroneous result was set aside. Controls were made for each organic and each surfactant providing a solution of just water and organic compound. We then noted the difference in the concentration of the organic compound in the vapor state between the organic compound-water system and the organic compound-watersurfactant system. The concentration of each organic compound in the vapor headspace of each flask was plotted against the surfactant concentration of each solution, and the series of curves in the appendix were developed.

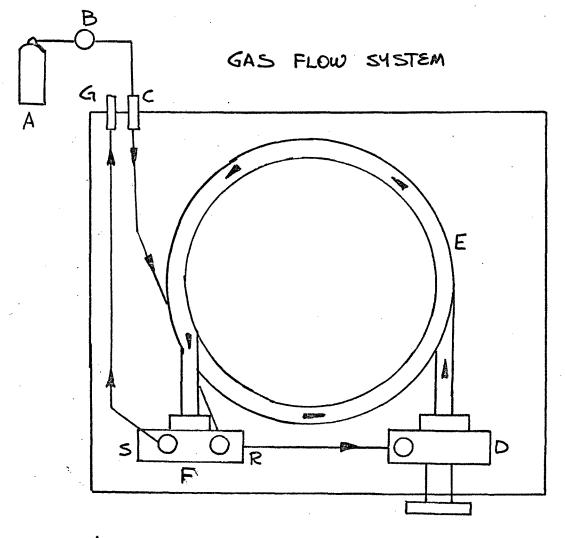
As was previously noted, the vapor pressure of a gas in a liquid phase equals the partial pressure of the gas in the gaseous phase upon saturation of the liquid. The partial pressure of the gas decreases as the vapor pressure increases until equilibrium is achieved in a closes system. The closed system is our 50 ml erlenmeyer flask and we note this reduction in partial pressure to be a reduction in concentration of the organic compound in the vapor headspace, thereby increasing its vapor pressure in the water-surfactant mixture σ increasing the amount of organic absorbed and the solubility of the organic in the system. The converse is

-33-



- A. CARRIER GAS (HELIUM)
- B. REGULATOR
- C. INJECTION PORT
- D. COLUMN
- E. DETECTOR
- F. RECORDER





A. HELIUM TANK

B. PRESSURE REGULATOR

C. INLET

D. INJECTION PORT

E. COLUMN

- F. DETECTOR
 - R. REFERENCE
 - S. SAMPLE

G. OUTLET

FIGUREG

also true, an increase in organic concentration in the vapor state would mean an increase in partial pressure and thus a reduction of the vapor pressure of the organic in the watersurfactant system, thereby reducing the amount of organic absorbed and denoting a reduction of solubility of the organic in the vapor, the lesser amounts of organic entered into solution with the water. Or the lower the concentrations of organic compound in the vapor state, the greater amounts of organic entered into solution with the water. By comparing the original concentration of the organic in the vapor state of the control sample to the concentrations of organic in the vapor state of each sample containing an increasing amount of surfactant, we determined the differences in solubility of the organic compound in the water-surfactant solution.

Our curves exhibit these differences in solubility quite readily and the following discussion will try to develop the patterns and trends of the various organics' when effected by the different surfactant types used. Tables of the data obtained are included in the appendix.

The following immiscible or partly miscible organics in water were examined to determine whether surfactants could affect this immiscibility.

- 1. Xylene
- 2. Toluene
- 3. Carbon Tetrachloride
- 4. Ethyl Acetate

5. Iso-propyl Alcohol

We used a reagent grade of organic compound and city water in the experiment. The practicality of a process depends on its feasibility on the commercial scale; and the large amounts of water necessary to operate any scrubber compounded by the need to keep costs as low as possible, makes it imperative for us to keep down the requirements of the scrubbing liquid, hence city water.

The above organics were "scrubbed" (i.e. meaning being acted upon by our experimental procedures) with varying concentrations of the following surfactant types:

> Anionic -- ethylene oxide based Anionic -- ethylene oxide based-linear Anionic -- sulfonate

Anionic -- hydrotrope

This limited surfactant range was used to determine the trends of the surfactant affects on the solubility of the organics in water.

We then proceeded to examine xylene's immiscibility with a wider range of surfactants under the same experimental conditions. These surfactants included:

A. Various alkyl sulfates

1. Fatty Alcohol

2. Fatty Ether

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B. Various sulfonates

1. Dodecylbenzene

2. Alkyl Benzene

3. Alkyl Carboxy

C. An Alkylolamide

1. Fatty Acids

D. A Hydrotrope

2.4

1. Xylene based

E. An Anionic-Nonionic

After much discussion, we analyzed the the data obtained in accordance with the above surfactant groupings. We found, generally, the surfactants to have an effect on the organic-water system. Therefore, to determine if these effects are common to all organics or all surfactants, or certain organics, or certain surfactants, or to just certain organic-surfactant systems, we felt this method of analization to be most appropriate.

Surfactant concentration for such a simple varied from 0% for the control cample to over 16%. Thus we feel we explored the possible ranges of surfactant concentrations that would be feasible in an actual scrubbing situation. That is, at greater surfactant concentrations, the amount of water would make the process impractical.

-37-

Ethylene oxide based surfactant

This surfactant is Sandopan DTC Gel Paste 6400-0-100, manufactured by Sandoz. This surfactant's effects on the solubilities of the above organic compounds can be seen in Figures 100, 104, 108, 112 and 116. Charts 100, 104, 108, 112, and 116 express percent changes of solubility for each organic in water at specific surfactant concentrations.

From Figure 100, the xylene vapor concentration for the xylene liquid to water concentration of lml to 19ml decreases, then increases and then decreases as the surfactant quantities are increased. When the xylene concentration was more than halved to 0.5ml xylene to 19.5ml water a gradual decrease in xylene vapor concentration was followed by a minimum at 4.8% surfactant. The solubility of xylene was increased about 18% at this point. A comparable increase in solubility at the lower xylene concentration of 17% occurred at 9.2% surfactant. This surfactant. This surfactant increased the solubility of xylene in water at nearly all concentrations.

A nearly identical course is set by isopropyl alcohol, Figure 116. The higher isopropyl alcohol in water concentration's vapor concentration decreases, shows an increase and then a decrease. The solubility is increased about 18% at 9.2% surfactant. The lower isopropyl alcohol concentration curve has two minima, increasing the solubility of iso-

-38-

propyl alcohol nearly 88% at 4.8% surfactant and 87% at 16.8% surfactant. This surfactant effected a large increase in the solubility of isopropyl alcohol in water after a slight variation increase at first. Large increases such as these warrant further investigation on a larger scale.

Carbon tetrachloride, Figure 104, exhibited similar results as xylene and iso-propyl alcohol at the concentration of lml organic and 19ml water. The same basic curve was developed: an initial increase followed by a decrease in solubility. However, although the decrease varies with surfactant concentration, the surfactant is generally a great hindrance to the solubility of carbon tetrachloride in water. A 57% decrease in solubility occurs at 8.8% surfactant concentration for the high CCl₄ to water system, and at the same surfactant concentration the low CCl₄ - water concentration system exhibited a decrease in solubility of 92%.

Initially this surfactant was a hindrance to the absorption of ethyl acetate and to toluene of higher concentrations as the surfactant concentration increased to about 4.8%. However, at this concentration a dramatic increase in the solubility of these organic compounds can be noted, see Figures 112 and 108. The ethylacetate increase in solubility in water is 55% at a surfactant concentration of 9.6% for the low ethylacetate concentration system; and 23% for the

-39-

high ethyl acetate concentration system at the same surfactant concentration. From Figure 112 we note a minimum at this 9.6% surfactant concentration and then both ethyl acetate concentrations show greater surfactant concentrations in water inhibiting further solubility of the ethyl acetate.

Toluene also shows a minimum at about 9.2% surfactant concentration. This increase in solubility is 39% for the high toluene concentration system and 18% when the toluene concentration was halved. At the low toluene concentration a gradual increase in solubility is accompanied by greater increases as the surfactant concentration increases.

Certain aspects of all the curves seem to be comparable to other aspects of the curves. Close examination shows that except for one or two points, the xylene, toluene, and iso-propyl alcohol curves are quite similar, exhibiting the same trends (i.e. increasing or decreasing solubility) at similar surfactant concentrations. All the organics tested, with the exception of carbon tetrachloride, had their solubilities in water increased to some extent through the use of this surfactant.

Also all the curves (see figures noted) of organic compound vapor concentrations versus surfactant concentration had a dramatic maximum or minimum occur between 4.8% and 9.2% surfactant concentration. This phenomena could be explained as the critical micelle concentration occurring

-40-

around the concentration. Figure 3 identifies the critical micelle concentration as the point where surfactant effects on water properties is drastically altered. The critical micelle concentration is the concentration where the maximum change in water properties occurs, thus it is logical for the greatest amount of absorption to occur at this point. If the properties of the water were changed to the extent that they are a hindrance to absorption or an aid to desorption, it is only proper that a maximum occur at the critical micelle concentration. The abrupt changes in solubility experienced by our data at a predictable concentration leads us to believe this theory true.

Water properties agreeable to ethyl acetate desorption seem to be effected by small amounts of surfactant increased and reached what we consider the critical micelle concentration at a point between 4.8 and 9.2%, the water properties are changed such that the absorption of the ethyl acetate occurs quite readily.

Examining the flasks and their contents gives no impression at this surfactant concentration of the critical micelle concentration, or other physical characteristics that may develop into a pattern. The xylene solutions are hazy at first and then clear up upon high surfactant concentrations (see Tables). The toluene solutions had similar physical characteristics as the xylene solutions: a light haze that

-41-

got denser followed by a clearing of the solution with added quantities of surfactant.

The carbon tetrachloride solution, upon the addition of 0.5 grams of surfactant was cloudy with a white residue on the bottom of the flask (possibly denoting supersaturation of the solution with surfactant or a reaction between the surfactant and the carbon tetrachloride forming a precipitate). Increasing the surfactant concentration changed the solution's appearance to a slight haze.

We could speculate that since all the above solutions were white hazy in appearance around the surfactant concentration range 4.8 - 9.2%, this must be the critical micelle concentration. At the critical micelle concentration the large number of micelles, or aggregate of moleculse, produce a translucent solution because of the reflection and refraction of light waves by these micelles.

However, we cannot conclude this to be true because of the ethyl acetate and iso-propyl alcohol solutions. These solutions produced a solution of one clear layer, even for the control, which was two clear layers for the other organic compounds; suggesting some solubility of these two organics before the tests began. Another reason for not stressing the physical appearance to explain our results or to find the critical micelle concentration is published data from the manufacturer, Sandoz notes the differences in solution appearances for a variety of compounds and Sando-

-42-

pan DTC Gel Paste concentrations. The appearance range from a haze for xylene in a 10% surfactant range (which does clear upon increased surfactant bearing out our findings), to clear for a solution of 5% NaOH and 1% surfactant, to a phase separation for a solution of mineral spirits and 5% surfactant. Obviously, for this surfactant, physical appearance has little meaning for the interpretation of the results.

Ethylene oxide based -- linear surfactant

This surfactant is Sandopan DTC Linear Gel 7445-121-5 manufactured by Sandoz. We must address ourselves to the fact that by solving an air pollution problem, we might be creating a water pollution problem. Besides the obvious, removing the organic emulsions formed from the water, the surfactant-water solution might create undesirable situations in the event water volumes for this scrubbing process are large.

This linear surfactant tested is more readily biodegradeable than its non-linear counterpart. Depending on the test method, the linear surfactant proved to be biodegradeable in excess of 90%. Using the river water die-away test after 15 days this surfactant was degraded 94% compared to a 48% degradation of the previously discussed surfactant.

-43-

Concentrations of organics in the vapor state decreased greatly in nearly all cases, thus, solubility was increased for nearly all tests with the specified organics except for CCl4 which showed a decrease in solubility. Note figures 103, 107, 111, 115 and 119 for the following discussion:

Xylene's solubility in water was increased dramatically. For the higher xylene in water concentration (lml xylene:19ml water) the solubility increase was 32% at 2.5% surfactant. This increase became smaller as the surfactant concentration increased to about 14% at 9.2% surfactant concentration. The low xylene to water ratio 0.15: 19.5 had similar characteristics but at different surfactant concentrations. Its curve had a minimum at a concentration of 4.8% surfactant concentration with the net result of 39% increase in solubility.

Ethyl acetate was absorbed more readily in water as the surfactant concentration increased. There is a direct proportionality involved between ethyl acetate solubility and surfactant concentration. For both ethyl acetate water system concentrations the increase in solubility continues as the surfactant concentration increases, such that at 16.7% surfactant concentration we note an 18% and 46% solubility increase for the high and low ethyl acetate to water ratios respectively. (see Figure 115).

-44-

Isopropyl alcohol, see Figure 119, exhibits diverse characteristics of solubility in water-surfactant solutions. For all concentrations of surfactant tested with the 1.0ml isopropyl alcohol : 19.0ml water ratio, the isopropyl alcohol's solubility was increased. Initially at 2.5% surfactant the solubility increased to 48%. The addition of greater amounts of surfactant proved to lessen this large increase in solubility. However at 9.2% surfactant the solubility increase is still 33%. At this same surfactant concentration for the 0.5ml isopropyl alcohol: 19.5 ml water ratio the increase in solubility was 50%. The lower water to isopropyl alcohol ratio at first shows a slight decrease in the amount of organic absorbed, followed by a sharp increase and finally decreasing by as much as 42% at 16.8% surfactant. Surfactant concentration greatly affects the solubility of isopropyl alcohol in water. We note that even slight changes in concentration produces large changes in the solubility of this organic in water. A 2.3% differential in surfactant concentration produced a 41% differential in solubility.

This characteristic of large differences in solubility with increasing surfactant concentration is also exhibited by toluene. Initially the lower and higher toluene concentrations exhibit different characteristics. This surfactactant proved to increase the solubility of toluene for the higher toluene concentration, but aided desorption

-45-

for the lower toluene concentration. See Figure 111. Surfactant concentrations up to over 5% aided desorption of the toluene from the water at a toluene concentration of 0.5:19.5. After 4.8% surfactant concentration, the two toluene concentrations showed sharp increases in solubility with added surfactant: nearly 43% and 21% increase at 9.2% surfactant for high and low toluene concentrations, respectively. Water requires larger amounts of this surfactant to improve toluene solubility in it than the other organics tested.

This surfactant was a hindrance to the solubility of carbon tetrachloride in water. The carbon tetrachloride left us no reason to believe this surfactant might aid its solubility. All tests showed an increase in CCl4 concentration in the vapor state thus denoting desorption of carbon tetrachloride from the water. The water properties were changed by the surfactant to cause an initial sharp rise in CCl vapor in the vapor state, followed by a gradual decrease as the surfactant concentration increased further. See Figure 107.

Again we noted the physical characteristics of each solution and tried to develop a connection between solubility changes, linear ethylene oxide surfactant concentration changes, and physical appearance.

The xylene solutions are slightly hazy at first followed by a denser haze and clearing of the solution. The to-

--46-

luene solutions had similar appearances. Ethyl acetate solutions of surfactant and water were clear: one clear layer for all surfactant concentrations. Iso-propyl alcohol solutions were also one clear layer for all concentrations. The carbon tetrachloride solutions exhibited a phase separation as a white residue settled on the bottom of all flasks with a quantity of surfactant.

There does not appear to be any dependence of solubility on physical appearance. The same physical appearances are not present for all organics or all surfactant concentrations. Therefore, determination of the critical micelle concentration of some other concentration where solubility increases are more apparent, is not feasible through physical charac^teristics of a solution of this surfactant.

Solubility effects do not occur more readily in a water-Sandopan DTC Linear gel surfactant concentration range of just under 5% through 10%. Nearly all minimum and maximums of the curves plotted fall within this surfactant range. This surfactant must affect the water properties to the utmost in this concentration range although from their physical appearance this coult not be ascertained.

Neither ethylene oxide based surfactant could change the properties of water to the extent needed to make carbon tetrachloride more soluble in it. Both proved to be a hindrance to CCl_h solubility and an aid to its desorption.

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Inspection of the curves, Figures 104 & 107, leave no reason for fuether investigation of these surfactants and carbon tetrachloride.

On the other hand xylene's solubility was improved by both linear and nonlinear ethylene oxide based surfactantsin water. The linear surfactant increased solubility to a greater extent over the nonlinear surfactant; 39% to 18% at comparable surfactant concentrations. Ethyl acetate, toluene, and iso-propyl alcohol also showed a general increase in solubility with the addition of the ethylene oxide based surfactants. And basically the solubility increases were no greater for the linear ethylene oxide than for the nonlinear surfactant.

Further examination of these graphs reveals to us a general similarity between curves for each organic tested. The high and low concentrations of each organic compound exhibited similar characteristics upon examination with water and the ethylene oxide surfactants. There is no reason to believe organic concentration greatly affects the effects of a solution of surfactant and water and organic. The solubility changes resulting from the surfactants' addition to water are not dependent on organic concentration in the system.

In nearly all instances outside of the carbon tetrachloride the trend of each curve for these two ethylene-

-48-

oxide based surfactants is for increased solubility. In some cases we note a gradual change in solubility as surfactant concentration increases and in others a slight change in surfactant quantity produces differences in solubility.

The ethylene oxide based surfactants have influenced the properties of water to effect the solubility of some organics in water to some extent. Our investigation continues with a variety of differently based surfactants as we search for optimum as well as conclusive results.

Sulfonates

The sulfonate surfactant tested withall the previously tested organic compounds was Ultrawet 1565 (45.D5,) manufactured by Arco Chemical Company. It is an anionic surfactant whose basic composition is sodium dodecylbenzene sulfonate. The effects of the other sulfonates were examined as they pertain to xylene. These are Ninate 401, another dodecylbenzene sulfonate, only instead of sodium being the cation, Ninate 401 has a calcium cation; Stepantex DA-52 which has an alkyl benezene organic base with an amine cation; and Stepantex WB-42, a sodium alkyl carboxy sulfonate 70% active. These three surfactants are manufactured by Stephan Chemical Company. These final three surfactants along with the Ultrawet 1565 offer a wide range of sul-

-49-

fonates with their various bases and cation combinations. Thus the latter examination of xylene with this scope of sulfonates gives us a clearer picture as to possible surfactant effects on immiscible organic compounds' solubility in water.

The effects of Ultrawet 1565 on the solubilities of the organic compounds tested in water willbe discussed first.

Carbon tetrachloride's solubility is affected by this surfactant. See Figure 105. The CCl_hconcentration in the vapor state decreased greatly at the initial surfactant concentration of 2.5%. Thus we note (see table 105) a solubility increase of 66% for the CCl_{j_1} in water concentration of 1:9 and 30% increase for the low CCl_{j_1} concentration. The solubility of CCl₁ in water is improved at larger surfactant concentrations, although to a lesser degree, until surfactant concentrations reach around 10%. After this point the surfactant causes a desorption of $\text{CCl}_{\underline{l}\underline{l}}$ from water providing a greater obstruction to the absorption of CCl_h by this water-surfactant solution than just plain water. From the curves it is seen that a change in CCl_{\downarrow} concentration does not greatly affect the effects of a surfactant-water solution on the solubility of CCl_{j_1} in it. The curve of the two CCl, concentrations are nearly identical to one another denoting this conception. There is, however, a greater increase in solubility for

-50-

the higher CCl_h concentration.

Isopropyl-alcohol has an initial increase of solubility in water with a surfactant concentration of 2.5%. See Figure 117. The isopropyl-alcohol concentration in the vapor state decreased for both concentrations of isopropyl alcohol and water. At the higher organic in water concentration the solubility increase is 12% and 50% for the lower concentration at the initial quantity of surfac-The solubility of isopropyl alcohol at the low contant. centration is improved but to a lesser degree as surfactant concentration increases until a concentration of 9.2% surfactant is reached. For the higher organic in water concentration, the solubility decreases after about 3.5% surfactant and continues decreasing to a minimum of 15% at 9.2%. After a 9.2% surfactant concentration the solubility of iso-propyl-alcohol increases and improves by as much as 40% at 16.8% surfactant for the 0.5:19.5 ratio of isopropyl alcohol to water.

Again we note, see Figure 117, the patterns of the effects of this surfactant on both concentrations of isopropyl-alcohol. Except for the size of the change, there appears to be no apparent difference in the effects of this surfactant on isopropyl-alcohol concentration.

This surfactant has similar effects on ethyl acetate's solubility in water as it does on isopropyl alcohol.

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and carbon tetrachloride. After an initial large increase in solubility at low surfactant concentrations, the improvement decreases and then is effected to a greater degree after a surfactant concentration of 9.2%.

Ethyl acetate in the wapor state is decreased by 23% for an organic to water ratio of 1:19 and 11% for an organic to water ratio of 0.5:19.5 at a surfactant concentration of 2.5%. Further increase in surfactant produces an even greater effect on the solubility of the higher ethyl acetate concentration up to 4.8%. The solubility at the lower concentration is unaffected by a surfactant range of 4.8 to 9.6%. The greatest change in solubility occurs at a surfactant concentration of over 40% for both ethyl acetate concentrations. See Figure 113. Similar characteristics of the curves of both ethyl acetate concentrations causes us to believe that surfactant effects on solubility are not dependent on the quantity of ethyl acetate in water.

Examining the curves for isopropyl alcohol and ethyl acetate. Figures 113 & 117, we note the similar characteristics this surfactant produces on both organic compounds. The same general properties are held by CCl₄ (Figure 105) for this surfactant as the previously mentioned organics except for at high surfactant concentrations.

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Toluene at its lower concentration of 0.5:19.5 in water is relatively unaffected by this surfactant. The largest change in solubility is only 5% at a surfactant concentration of a 4.8%, this decreases such that the toluene-water system's miscibility is unchanged. The most rapid change and increase in solubility occurs after 2.5%. This is also true for the higher toluene in water concentration where after the 2.5% surfactant concentration the greatest increase in toluene concentration in the vapor headspace occurs. Furthermore, this surfactant is an aid for desorption of toluene from the water-toluene mixture at the high toluene concentration, and this desorption increases as surfactant concentration increases.

With the above surfactant, xylene also showed no appreciable change in solubility. The lower xylene concentration system had its solubility (see Figure 101 and Table 101) increased 5% at 2.5% surfactant. This was the maximum value obtained as further increase in surfactant had lesser effects on the properties of the xylene-water mixture, until no effects could be determined. The higher concentration xylene system peaked at a 26% decrease in solubility at 4.8% surfactant and then declined as further increases in surfactant concentration proved to be less of a hindrance to solubility. This Ultrawet 1565 surfactant is a sodium dodecylbenzene sulfonate and the results obtained

-53-

we believe are comparable to Ninate 401, another dedecylbenzene organic based sulfonate only with a calcium cation instead of sodium. See Figure 126. The effects of both surfactants on xylene are similar except Ninate 401 produces much more drastic results. The lower concentration of xylene in water had its solubility changed for the better by 21% at 4.8% surfactant. At other surfactant concentrations the increase in solubility was not as great. The higher xylene in water concentration produced the opposite results with this surfactant as it did with the previous surfactant. There is a steady rise in xylene concentration in the vapor state, denoting desorption, until it reaches a 47% increase at 9.1% surfactant. The drop in surfactant effects that follows is dramatic; in fact, for both dodecylbenzene surfactants, the effects on water properties to influence absorption of xylene is diminished at higher concentrations. This is true for both concentrations of xylene in water as at high dodecylbenzene surfactant concentrations there is relatively no change in solubility.

The affects of other sulfonated surfactants on xylene solubility in water was explored. Stepantex WB-42 the soldium alkyl carboxy sulfonate (see Figure 123) influenced a greater absorption of xylene by water. For both xylene concentrations there is an initial increase in solubility

-54-

followed by a decline in the size of this increase as larger amounts of surfactant are added to the system. The lower xylene concentration curve shows two minima for xylene concentrations in the vapor state. A 31% increase in solubility at 2.5% surfactant and 49% increase at 16.7%. The higher xylene concentration also varies dramatically with surfactant concentration.

This is true for the various concentrations of Stepantex DA-52 tested. Although the higher concentration of xylene in water proved this surfactant to have adverse effects on xylene solubility, after an initial decrease of 59% at 2.5% surfactant, these decreases were relatively small at greater surfactant concentrations. The lower concentration of xylene in water system shows xylene solubility to be unaffected by this surfactant until the surfactant concentration surpasses 2.5%. Xylene solubility in water is then improved by as much as 18% as the surfactant concentration increases.

We note from these surfactants that the initial xylene concentration in water is a factor when determining surfactant effects on the solubility of xylene in water. Figures 101 & 126 exhibit this fact. From Figure 123 we might suspect the same, however, both xylene solubility and the concentration of this surfactant could be more significant than previously tested surfactants. It seems from

-55-

these results that the type of surfactant is just as important as surfactant concentration when trying to influence the properties of the xylene-water system. Whereas, over \mathfrak{W} of all tests of xylene with sulfonate surfactants resulted in improved solubility, the variables are considerable and seem to be quite specific. That is, a certain xylene concentration might need a specific concentration of a specific sulfonate surfactant in order to effect the required results.

We examined the appearance of these samples and found no evidence of physical appearances affecting specific results. Ethyl acetate and isopropyl alcohol exhibit similar physical characteristics of a clear solution for all organic and surfactant concentrations. Carbon tetrachloride had a phase separation--a clear solution with a white residue on the bottom. Toluene and xylene for the Ultrawet 1565 produced hazy solutions for the surfactant ranges tested.

Xylene, water, and Stepantex WB-42 initially appeared as a grayish milky white solution and gradually changed with increased surfactant concentration. Its appearance went from milky white to a light off yellow solution. Stepantex DA-52, xylene, and water solutions were at first milky white at a 2.5% surfactant and the solution's

-56-

appearance became off white with additional surfactant. The solution was transformed into an amber gel at a surfactant concentration of about 16.8%. Ninate 401, xylene and water effected a phase separation. Initially we noted a mazy solution with a white and yellow residue on top. With increased surfactant this residue turned more yellow, then into a hazy yellow gel, and then a clear solution surrounding a yellow gel with a white solid residue on top.

The physical characteristics were unaffected by organic concentration. From Tables in the Appendix we see the slight differences that did appear.

In nearly all cases the solubility results were not dependent on organic concentration, however, we note the irregularities that occured with the latter surfactants discussed and xylene concentration.

Most activity for the Ultrawet 1565 surfactant occurred in a concentration range of 2.5-4.8%. Within this range we note an increased number of minima and maxima on our curves denoting drastic changes in water properties affecting solubility. Whether this is the range in which the cmc falls we have not determined. As noted physical characteristics of the different organic solutions exhibited no similarities to suggest a developing trend that might allow us to make such an assumption.

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For all the surfactants tested there was a general influence on the physical properties of water to allow for a greater organic solubility in water.

Hydrotropes

All the previously mentioned organics were examined with surfactant 40SX as manufactured by the Arco Chemical Company. Xylene was further examined for solubility effects by Stepanate AM as manufactured by Stepan Chemical Company. Surfactant 40SX is a sulfonate hydrotrope with xylene as the organic base and sodium the cation. Stepanate AM is a similar hydrotrope with a sodium cation and xylene organic base.

The 40SX surfactant decreased the solubility of xylene in water at all times. At the higher xylene concentration we note the decrease in solubility is directly proportioned to the increase in surfactant concentration. Our graph (Figure 102) showing a maximum 42% decrease at 9.2% surfactant. The lower xylene concentration fared better, in that after a large initial decrease of 28% solubility at 2.5% surfactant, the decreasing diminished and leveled off at a decrease in xylene solubility approximately 15%.

A similar decrease in xylene solubility resulted with the lower xylene in water concentration system and Stepanate AM. A sharp decrease of 23% at 2.5% surfactant

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is followed by results showing practically no surfactant effects at 4.8% surfactant. Variations in solubility of xylene continue with increased surfactant concentrations, however these variations are rather small. The higher xylene concentration system (lml:19ml) improved in the amount of xylene absorbed in the water. Variations are sharp as a slight increase in this surfactant produced a wide difference in xylene solubility.

Except for the higher xylene concentration and Stepanate AM system, we noted a decrease in xylene solubility for these surfactants. Since these are xylene based surfactants the results could have been affected by a xylene concentration already in the water. In the control flasks without the surfactant, we determined the xylene concentration, and then with the surfactant we did the same. Obviously in those flasks with xylene, water, and surfactant there is more xylene than in those without a surfactant. As a result of partial pressures differences, xylene from the surfactant solutions might be forced out of solution to add to the xylene concentration in the vapor state. Thus when passing a sample through the gas chromatograph a larger xylene concentration is recorded for surfactant samples. The possibility also exists that these surfactants are just detrimental to xylene solubility in water, that they change the water's properties to effect the immiscibility of xylene in water.

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The other organics were only tested with surfactant 40SX and the results, while mixed, showed a general trend towards improvement of solubility in water.

Carbon tetrachloride showed a gradual increase in solubility over the surfactant concentrations used. The higher carbon tetrachloride system's solubility was relatively unaffected by the surfactant until a concentration over 2.5% is reached. After this point, increases in CCl_{l_1} solubility are directly proportional to surfactant increases reaching a maximum of 21% improvement at 16.2% surfactant. The lower CCl₁ concentration system initially increases insolubility by about 19% at 2.4% surfactant. The solubility of $\mathtt{CCl}_{\underline{h}}$ is improved with further surfactant increases, but this improvement waries without any consistency. Both concentrations of CCl₁ show solubility improvements in the same order of magnitude and there is a relationship between CCl_{h} concentration, surfactant concentration, and the size of the solubility improvement.

For the high isopropyl alcohol concentration system, the solubility as well as magnitude of solubility increases are dependent on surfactant concentration increases. At 2.5% surfactant concentration the isopropyl alcohol solubility improvement is 24%. This improvement varies unpredicably with further surfactant increases, as declines and increases in solubility improvement magnitudes are noted

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(see Figure 118). When the isopropyl alcohol concentrations was halved, the solubility was unaffected by small amounts of surfactant. In fact the solubility of isopropyl alcohol in water is generally unchanged at the lower concentration until a surfactant concentration of around 9% is reached. At this concentration the amount of isopropyl alcohol in the vapor state is nearly doubled denoting the affects of the surfactant as a hindrance to solubility.

Toluene's solubility in water at the lower concentration of toluene to water 0.5:19.5 improved by 34% at a 2.5% surfactant concentration. A decline in improvement occurs at 4.8% and then increases to 22% at 9.2% surfactant. Thus the magnitude of solubility improvement is highly dependent on the surfactant concentration. This is also true for the higher toluene concentration system (see Figure 110). Although there is a decrease in solubility, the magnitude of this change is also dependent on surfactant concentration with large variations accompanying slight changes in surfactant quantities.

Similar results were obtained by the ethyl acetate system. The high ethyl acetate to water ratio system showed ethyl acetate's solubility decrease by 29% at 2.5% surfactant. The size of this decrease remained stable with increased surfactant until 9.6% surfactant concentration.

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However, with a surfactant concentration of 16.7% surfactant affects on water properties to effect absorption are diminished. This is not apparent for the lower ethyl acetate concentration. In these tests the ethyl acdtate's solubility was improved by 32% at 2.5% surfactant and continued to improve, although slightly, with increased surfactant concentration.

We note for both toluene and ethyl acetate the high organic in water ratio is affected by the surfactant in such a manner that there is more organic in the vapor state, suggesting the surfactant to be a hindrance to solubility at higher concentrations. There is a solubility improvement for the organics when the surfactant is added to the water of the lower organic to water ratio tested.

We note for the surfactant 40=SX that the concentration range between 2.5 and 4.8% produces the most radical differences in water-organic absorption properties. We might suggest this concentration to be the critical micelle concentration, since in order for these radical differences to occur the water must be effected to a maximum and at this point the critical micelle concentration occurs.

Appearances of the solutions do not suggest any trends and/or critical micelle concentration. All the physical characteristics of the original five organics

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tested--xylene, toluene, ethyl acetate, carbon tetrachloride and isopropyl alcohol -- were the same for surfactant 40 SX as for Ultrawet 1565 and the ethylene oxide compounds. Please see tables. Stepanate AM surfactant produced unusual characteristics for the xylene water surfactant solution (see Table 127,) however there does not seem to be any connection between solubility, water and organic properties, and solution physical appearances. Physical characteristics in some cases--xylene, toluene, CCl_4 -are dependent on surfactant concentration. Ethyl acetate and isopropyl alcohol show no such dependencies.

We cannot make the general statement that solubility effects produced by a surfactant are independent or organic concentration. These surfactants effected solubility changes which were dependent on organic concentrations and surfactant concentrations, thus making predictability of an optimum system difficult and nearly impossible. Such a dual dependency for optimal results would make water scrubbing or organic gases impossible since gas concentrations will change quite readily, and to constantly monitor the gas concentration to effect a surfactant concentration change would be unfeasible both on the technical as well as economic levels.

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Alkyl Sulfates

The following surfactants tested are manufactured by Stepan Chemical Company. Stepanol WAT has a fatty alcohol organic base and TEA cation. Steol KS-460 has a fatty ether organic base and sodium cation. Xylene was the mly organic tested with these surfactants. The general characteristics of the affects on the solubility of xylene are identical for each surfactant, see Figures 120 and 121. There is the initial increase of xylene concentration in the wapor state, (i.e. denoting a reduction in solubility,) followed by a decline in xylene vapor concentration and to finally increase with increasing surfactant concentration.

Stepanol WAT effects an initial 70% decrease in xylene solubility at 2.5% surfactant for the high 1:19 xylene to water ratio. With further addition of surfactant to a 4.8% concentration, the decrease in solubility declines to about 45%. At this point a minimum is reached and additional surfactant concentrations further decrease the solubility of xylene in water. The low xylene to water concentration 0.5 to 19.5 exhibited not so drastic effects by the surfactant. Although the trends were similar, there is merely a 7% decrease in solubility at 2.5% surfactant. The increase in xylene absorption by water that follows reaches a minimum

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at 4.8% surfactant and results in a 15% increase in xylene solubility. However, after this surfactant concentration, solubility of xylene is indirectly proportional to surfactant concentration. That is, an increase in surfactant concentration produces a decrease in solubility attaining a maximum decrease of 31% at 16.7% surfactant.

Steol KS-460, although effecting various results, did not cause an increase in xylene solubility. For the l:19 xylene to water ratio, a peak of 69% increase in xylene vapor concentration is attained at 2.5% surfactant. The vapor concentration is increased by all surfactant concentrations tested, although the magnitude of these increases varied. Solubility is decreased by only 22% at 4.8% surfactant, but again decreases with increased surfactant after this point. Xylene in water at a concentration of 0.5:19.5 exhibit similar effects by this surfactant. The maximum reduction in solubility of 87% occurs at 4.8% surfactant concentration. A drop off in this reduction is effected at 9.1% surfactant and continues as the solubility decreases with further surfactant increases.

By observing the data produced, xylene concentration is mot a factor in an alkyl sulfate's ability to effect solubility. Both concentrations of both surfactants tested have highly similar characteristics. Xylene to water

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concentrations are different only with respect to magnitude of the dolubility change, rather than the change itself. Both surfactants effect drastic changes in solubility at a surfactant concentration range between 2.5-4.8% denoting large water property changes and possibly marking the critical micelle concentration.

Other physical characteristics of these solutions did not exhibit any properties which would lead us to suspect an increase in surfactant past the critical micelle concentration (about 2.5-4.8%) would effect further solubility changes. The Steol KS-460 surfactant-water-xylene system produced milkly white solutions for all surfactant concentrations until it turned clear upon the addition of 16.7% of the surfactant. We note the Steol KS-460 solutions were predominately milkly white through the concentration range where a variation in surfactant to a slight degree, produced large changes in xylene absorption by water.

This result is duplicated by Stepanol WAT. For the concentration range of 2.5 to 4.2% we observe a hazy solution with a white residue on top, thus possibly denoting the cmc, and at these concentrations our most serious changes occurred. Further increasing the surfactant concentration turned the solution clear and reduced the amount of white residue on top until there was a clear solution at 16.7% surfactant. From these surfactants we can suggest the

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interrelationship of solution physical appearance and its characteristics (i.e. the cmc) to effect miscibility of xy-lene.

As much as these alkyl sulfates do affect water properties to effect changes in xylene solubility, they do not result in increased xylene solubility in water. In fact they prove to be a hindrance to the absorption of xylene by water and prove to further aid the immiscibility of xylene to water.

Alkylolamides

The alkylolamide tested with xylene was manufactured by the Stepan Chemical Company. Ninol 1281 has an organic base of fatty acids.

Solubility of xylene in water was initially decreased by around 8% for the higher xylene in water concentration. The solubility of xylene in the water-surfactant solution begins to increase after a 4.8% surfactant concentration is reached and continues until a 14% increase is attained at 9.2%. Further surfactant increases decrease the solubility of xylene. The lower xylene to water ratio follows suit. The initia! decrease in solubility is followed by an increasing insolubility to about 5% at a 4.8% surfactant concentration. Again solubility deceases with further in-

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creases in surfactant.

The properties exhibited by these water-xylenesurfactant systems seem to be pretty much universal -there is a surfactant concentration in water, possibly the cmc, which is favorable to the absorption of xylene by water to a greater extent than just xylene in water.

This alkylolamide produced hazy solutions with white residues for surfactant concentrations up to about 5%. After which the solutions turned yellowish and then into gels.

As in all previous cases the organic concentration had very little affect on the physical appearances of the solutions. And in this instance both xylene in water concentrations were dependent on surfactant concentration to the same degree.

Emulsifiers

The emulsifier used with xylene was Toximul R as manufactured by Stepan Chemical Company. It is an anionicnonioic emulsifier and produced some interesting results.

For both xylene in water concentrations there are very small affects produced by nearly all surfactant concentrations. The high concentration of xylene at first exhibits a reduction in xylene concentration in the vapor

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headspace, therefore an increase in solubility by 7%. This figure decreases with increasing surfactant until no distinguished at 9.1% (see Table 124). Following this point, surfactant effects increase and we note a 36% xylene solubility increase at 16.7% surfactant.

The lower xylene-water concentration system initially decreases in solubility by about 10% and remains unaffected by further surfactant increases up through 9.1% surfactant. As with the previously discussed xylene concentration, after this point solubility increases and reaches a maximum improvement of 2% at 16.7%. Although this improvement is small in comparison with the improvement noted for the higher xylene concentration, we must acknowledge the trends developing for this surfactant and make note of the increased solubility at a relatively high concentration of 16.7%.

This 16.7% concentration could be the critical micelle concentration for this surfactant. Regretably we did not foresee this development to examine higher surfactant concentrations which would have given us more data. Physical appearances do not prove to be of any significance. Solutions of xylene, water and Toximul R are milkly white until 4.8% surfactant is reached, then a yellow tinge develops to the milky white solution and finally we have a translucent solution with a yellow tinge. Since after the development of the yellow tinge the beginning of the solubility

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increases occurs, we suggest this yellow tinge is the formation of the micelles resulting in the cmc at 16.7%.

What we are suggesting is that if the cmc is known, and if this is where the solubility increases are effected, then the problem of scrubbing organics from an air stream with a water-surfactant solution is reduced to producing a scrubbing liquid of proportionate amounts of water and surfactant.

Therefore, if the minimums on our graphs (denoting increases in solubility) are in actuallity the critical micelle concentration of the surfactant we have proved our theory of surfactants affecting water properties to effect the solubility of certain immiscible or partly miscible organics. If these minima are not the individual cmc of each surfactant tested, we have still proved our theory of immiscibility correct, but further investigation at higher surfactant concentrations may provide the cmc of that solution and the optimum xylene in water solubility should result.

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CONCLUSION

It is clear from our results that the solubilities of certain immiscible and partly immiscible organics in water can be affected surfactants. Depending on the surfactant type, surfactant concentration, and in some instances the organic concentration, the solubility of these organics in water can be increased dramatically. Therefore the scrubbing of an air stream including organics with a water-surfactant solution is highly possible. However it is also evident that for each particular organic a specific surfactant and a specific surfactant-in-water concentration is necessary to obtain optimum results.

For each surfactant there is a concentration, the critical micelle concentration, where water properties are affected to the greatest degree and evidence of this is exhibited by our results. There is a surfactant concentration, whether favorable or unfavorable, where the surfactant-water system affects the solubility of the organics to the utmost. Our curves show these points with minima and maxima.

The activity that occurs at these points should be explored to a greater extent. By finding the surfactant concentration which effects the greatest absorption of a particular organic by water, we can seed the scrubbing water with the surfactant to the required concentration and thus "clean" an air stream polluted with organic vapors.

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Warranting further examination is the possibility or recirculating the scrubbing water-surfactant-organic solution. Because wet scrubbers may require vast amounts of scrubbing liquid, the scrubbing liquid is usually recirculated to reduce costs. However the efficiency of scrubbing declines to a point where recirculation becomes impractical. In our investigations we did not explore the absorption of organics by an organic-water-surfactant solution, which we feel possibly would become more efficient as the organic absorbed is increased. Since these surface active agents are organic compounds, and they do affect water properties such as surface tension and interfacial tension, the absorption of an organic pollutant would cause further effects, preferably to induce the absorption of more organic compound.

In most of our experiments the organic to water concentration was relatively unimportant. That is, the effects of a particular surfactant and surfactant concentration are not dependent on the initial organic concentration. Although the organic absorbed differentials are varied, the relative magnitude of organic absorbed by the water and therefore surfactant effects are similar for different organic concentrations.

The solubility of each organic---xylene, toluene, carbon tetrachloride, ethyl acetate, and isopropyl alcohol---

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in water can be improved by the addition of a surfactant. Not all surfactants are useful with all organics. Some organics' solubilities are decreased, some are unaffected, and others are increased with the addition of certain surfactants. Different surfactant's effect different organics to different extents. All the organics examined showed a solubility improvement with one α more of the surfactants tested.

We believe air experiments justify further examination under actual operating conditions, i.e. a wet scrubber. We have effected solubility in water changes for the organics tested, but only with a packed tower will we be able to predict further feasibility.

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APPENDIX

RETENTION TIMES

Organic Compound	Time in gas chromatograph before recording
Xylene	7.4 minutes
Toluene	4.2 minutes
Carbon Tetrachloride	2.3 minutes
Ethyl Acetate	2.1 minutes
Iso-propyl Alcohol	1.6 minutes

KEY TO FLASK NUMBERING SYSTEM

First Diget	Organic type
Second Diget or Letter	Surfactant type
Third Diget	Surfactant concentration
Fourth Diget	Flask differences for surfactant concentrations

ORGANIC NUMBERING SYSTEM

ZERO .	•	•	•	÷	•	. •	•	•	•	•	•	•	•	•	•	•	Xylene
ONE .	•	•	•	•	•	•	•	•	•	•	٠	•	•	•	•	•	Toluene
TWO .	٠	•	•	•	•	•	•	•	•	•	•	•	•	٠	•	•	Carbon Tetrachloride
THREE	•	٠	•	•	•	•	٠	•	•	•	•		•	•	•	•	Ethyl Acetate
FOUR	•	•	•	•	•	•	•	•	•	٠	•	•	•	•	٠	•	Iso-propyl Alcohol

SURFACTANT NUMBERING SYSTEM

•	1	•	•	•	•	•	•	•	•	•	•	•	•	•	•	٠	•	Sandopan DTC Gel Paste*
	2	•	•	•	.	•	٠	•	•	•	•	٠	•	•	•	•	•	Ultrawet 1565 (45.DS)**
	3	•	•	•	•	٠	•	•	•	٠	•	0	•	•	•	•	•	40 SX-Lot #5212**
	4	•	•	•	•	•	٠	•	٠	•	•	•	•	•	•	•	•	Sandopan DWC Linear Gel*
	A	•	•	•	٠	٠	•	•	•	•	•	•	•	٠	•	•	•	Stepanol WAT***
	B	•	•	•	•	•	٠	٠	•	•	٠	•	٠	•	•	•	•	Steol KS-460***
	C	•	• •	•	•	•	•	٠	•	•	¢	•	•	٠	٠	•		Ninol 1281***
	D	٠	•	٠	•	•	٠	•	•	•	٠	•	•	•	٠	٠	•	Stepantex WB-42***
	E	٠	•	•	•	٠	•	•	e	٠	•	o	٠	•	٠	•		. Toximal R***
	F	•	•	o	•	•	•	•	0	•	٠	•	•	٠	•	•		Stepantex DA-52***
ł	G	.•	•	•	٠	٠	•	•	•	•	•	•	•	٠	٠	•		Ninate 401***
	H	•	•	٥	•	•	•	•	•	٠	٠	•	•	•	٠	. •		. Stepanate AM***
					*]	Ma	nu	fa	cti	ur	ed	by	7	Sai	nd	oz		
		**Manufactured				b	by Arco Chemical Company					emic al Company						
				**	**]	Mai	nu	fa	ct	ur	ed	bj	Ţ	St	ep	ha	n	Chemical Company

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TABLES OF RESULTS

T	ABLE	100

				1. A. C. A.			
	Bottle Number	Water	Organic**	Wetting Agent*	Appearance	Organic Vapor Concentration	
		<u>(ml)</u>	<u>(ml)</u>	(grams)		(grams/cc)	
	011A 011B 011C	^{***} 19 19 19	1 1 1	0 0 0	clear with two layers	2.174 x 10 ⁻⁵ 2.20 x 10 ⁻⁵ 1.91 x 10 ⁻⁵	
	Wetting Concent		0.0000		Average	2.187 x 10 ⁻⁵	
	012A 012B 012C	19 19 19	1 1 1	0.5 0.5 0.5	hazy	1.933 x 10 ⁻⁵ 2.356 X 10 ⁻⁵ 1.958 x 10 ⁻⁵	
•	Wetting Concent		0.0246	··-	Average	1.946 x 10 ⁻⁵ .	
	013A 013B 0130	19 19 19	1 1 1	1.0 1.0 1.0	denser haze	2.635×10^{-5} 1.678 $\times 10^{-5}$ 2.176 $\times 10^{-5}$	
	Wetting Concent		0.0479		Average	2.406 x 10 ⁻⁵	
	014A 014B 014C	19 19 19	1 1 1	2.0 2.0 2.0	still denser haze	1.874×10^{-5} 1.74×10^{-5} 1.51×10^{-5}	
-	Wetting	g Agent cration	0.0914		Average	1.807 X 10 ⁻⁵	

*Sandopan DTC Gel Paste 6400-0100 **Xylene .

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Bot Num		Water	Organic**	Wetting Agent*	Appearance	Organic Vapor Concentration
		<u>(ml)</u>	<u>(ml)</u>	(grams)		(grams/cc)
0	15A 15B 15C	^{***} 19.5 19.5 19.5	0.5 0.5 0.5	0 0 0	clear with two layers	2.54 x 10 ⁻⁵ 1.752 x 10 ⁻⁵ 2.176 x 10 ⁻⁵
		Agent	0.0000		Average	2.353 x 10 ⁻⁵
0	16A 16B 160	19.5 19.5 19.5	0.5 0.5 0.5	0.5 0.5 0.5	hazy	1.813 X 10 ⁻⁵ 2.272 X 10 ⁻⁵ 2.78 X 10 ⁻⁵
		Agent cration	0.0244		Average	2.288 x 10 ⁻⁵
0	17A 17B 170	19.5 19.5 19.5	0.5 0.5 0.5	1.0 1.0 1.0	denser haze	2.082 X 10 ⁻⁵ 1.813 X 10 ⁻⁵ 1.933 X 10 ⁻⁵
		g Agent cration	0.0478		Average	1.943 x 10 ⁻⁵
0	18Å 18B 18C	19.5 19.5 19.5	0.5 0.5 0.5	2.0 2.0 2.0	still denser haze	2.015 X 10 ⁻⁵ 2.12 X 10 ⁻⁵ 1.474 X 10 ⁻⁵
		g Agent tration	0.0913		Average	2.067 x 10 ⁻⁵

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*Sandopan DTC Gel Paste 6400-0-100 **Xylene

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TABLE 101

Bottle Number	Water (ml)	Organic** <u>(ml)</u>	Wetting Agent* (grams)	Appearance	Organic Vapor Concentration (grams/cc)
021A 021B 021C	*** 19 19 19	1 1 1	. 0 0 0	clear with two layers	1.752 x 10 ⁻⁵ 2.455 x 10 ⁻⁵ 2.056 x 10 ⁻⁵
	g Agent tration	0.0000		Average	2.088 x 10 ⁻⁵
022A 022B 022C	19 19 19	1 1 1	0.5 0.5 0.5	haze	2.205 x 10 ⁻⁵ 2.239 x 10 ⁻⁵ 2.470 x 10 ⁻⁵
	ng Agent	0.0246	•	Average	2.222 x 10 ⁻⁵
023A 023B 0230	19 19 19	1 1 1	1.0 1.0 1.0	denser hase	$\begin{array}{r} 2.119 \times 10^{-5} \\ 2.648 \times 10^{-5} \\ 2.66 \times 10^{-5} \end{array}$
	ng Agent ntration	0.0479		Average	2.654 x 10 ⁻⁵
024A 024B 024C	19 19 19	1 1 1	2.0 2.0 2.0	still denser haße	2.356×10^{-5} 1.715 $\times 10^{-5}$ 2.119 $\times 10^{-5}$
	ng Agent ntration	0.0914		Average	2.238 x 10 ⁻⁵

*Ultrawet 1565 (45.DS) **Xylene

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	mber	Water (ml)	Organic** (ml)	Wetting Agent* (grams)	Appearance	Organic Vapor Concentration (grams/cc)
·	025A 025B 0250	³⁴ 19.5 19.5 19.5	0.5 0.5 0.5	0 0 0	clear with two layers	$\begin{array}{r} 2.445 \times 10^{-5} \\ 2.60 \times 10^{-5} \\ 2.345 \times 10^{-5} \end{array}$
		g Agent tration	0.0000		Average	2.463 x 10 ⁻⁵
	026A 026B 026C	19.5 19.5 19.5	0.5 0.5 0.5	0.5 0.5 0.5	haze	1.994 x 10 ⁻⁵ 2.385 x 10 ⁻⁵ 2.300 x 10 ⁻⁵
		g Agent tration	0.0244		Average	2.342 x 10 ⁻⁵
	027A 027B 027C	19.5 19.5 19.5	0.5 0.5 0.5	1.0 1.0 1.0	still denser haze	2.356 X 10 ⁻⁵ 2.965 X 10 ⁻⁵ 2.42 X 10 ⁻⁵
• • •		g Agent tration	0.0478		Average	2.388 x 10 ⁻⁵
	028A 028B 028C	19.5 19.5 19.5	0.5 0.5 0.5	2.0 2.0 2.0	still denser haze	2.575×10^{-5} 2.43 $\times 10^{-5}$
	Wettin Concen	g Agent tration	0.0914		Average	2.502 X 10 ⁻⁵

*Ultrawet 1565 (45.DS) **Xylene

Bott Numbe		Organic** (ml)	Wetting Agent* (grams)	Appearance	Organic Vapor Concentration (grams/cc)
03 03 03	1B 19	1 1 1	0 0 0	clear with two layers	1.97 x 10 ⁻⁵ 1.45 x 10 ⁻⁵ 0.918 x 10 ⁻⁵
We Co	tting Agent ncentration	0.0000		Average	1.710 x 10 ⁻⁵
03 03 03	2B 1 9	1 1 1	0.5 0.5 0.5	haze	1.91 x 10 ⁻⁵ 2.345 x 10 ⁻⁵ 1.765 x 10 ⁻⁵
	tting Agent ncentration	0.0246	.*	Average	1.837 X 10 ⁻⁵
03 03 03	3B 19	1 1 1	1.0 1.0 1.0	denser haze	2.235 X 10 ⁻⁵ 2.345 X 10 ⁻⁵ 1.427 X 10 ⁻⁵
	tting Agent ncentration	0.0478		Average	2.290 x 10 ⁻⁵
03 03 03		1 1 1	2.0 2.0 2.0	still denser haze	1.933 x 10 ⁻⁵ 2.331 x 10 ⁻⁵ 2.540 x 10 ⁻⁵
	tting Agent ncentration	0.0913		Average	2.435 x 10 ⁻⁵

*40SX--Lot#5212 **Xylene

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	Bottle Number	Water (ml)	Organic** (ml)	Wetting Agent* (grams)	Appearance	Organic Vapor Concentration (grams/cc)
	035A 035B 0350	19.5 19.5 19.5	0.5 0.5 0.5	0 0 0	clear with two layers	$\begin{array}{r} 2.49 \times 10^{-5} \\ 2.187 \times 10^{-5} \\ 2.065 \times 10^{-5} \end{array}$
	Wetting Concent	Agent tration	0.0000	•	Average	2.126 x 10 ⁻⁵
	036A 036B 0360	19.5 19.5 19.5	0.5 0.5 0.5	0.5 0.5 0.5	haze	2.660 x 10 ⁻⁵ 2.780 x 10 ⁻⁵ 1.812 x 10 ⁻⁵
		g Agent tration	0.0244	· .	Average	2.72 x 10 ⁻⁵
	037A 037B 0370	19.5 19.5 19.5	0.5 0.5 0.5	1.0 1.0 1.0	denser haze	2.50 X 10^{-5} 2.477 X 10^{-5} 2.356 X 10^{-5}
		g Agent tration	0.0478		Average	2.444 x 10 ⁻⁵
-	038A 038B 038C	19.5 19.5 19.5	0.5 0.5 0.5	2.0 2.0 2.0	still denser haze	1.994 X 10 ⁻⁵ 2.356 X 10 ⁻⁵ 2.518 X 10 ⁻⁵
		g Agent tration	0.0913		Average	2.437 x 10 ⁻⁵

*40SX--Lot#5212 **Xylene

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	ottle umber	Water (ml)_	Organic** (ml)	Wetting Agent* (grams)	Appearance	Organic Vapor Concentration (grams/cc) X 10 ⁻⁵
	041A 041B 041C	²⁴ 19 19 19	1 1 1	0 0 0	clear with two layers	2.065 1.330 2.633
•		g Agent tration	0.0000		Average	2.351
۰.	042A 042B 042C	19 19 19	1 1 1	0.5 0.5 0.5	haze	1.50 2.540 1.691
·		g Agent tration	0.0246	- - -	Average	1.595
	043A 043B 043C	19 19 19	. 1 1 1	1.0 1.0 1.0	denser haze	1.50 1.933 1.933
•		g Agent tration	0.0479		Average	1.933
	044A 044B 044C	19 19 19	1 1 1	2.0 2.0 2.0	still denser haze	1.209 1.875 2.285
<i></i>		g Agent tration	0.0914	· .	Average	2.030

*Sandopan DTC Linear Gel 6445-121-5 **Xylene

	Bottle	Water	Organic**	-	Appearance	Organic Vapor	
	Number	<u>(ml)</u>	<u>(ml)</u>	Agent* (grams)		Concentration (grams/cc)X_10	5
	045A 045B 0450	** 19.5 19.5 19.5	0.5 0.5 0.5	0 0 0	clear with two layers	3.240 3.190 2.730	
	Wetting Concent		0.0000		Average	3.215	
•	046A 046B 046C	19.5 19.5 19.5	0.5 0.5 0.5	0.5 0.5 0.5	haze	2.610 2.961 3.165	
	Wetting Concent		0.0246	Č.	Average	3.063	
	047A 047B 047C	19.5 19.5 19.5	0.5 0.5 0.5	1.0 1.0 1.0	denser haze	2.260 3.240 1.631	
	Wetting Concent	Agent	0.0479		Average	1.945	
	048A 048B 048C	19.5 19.5 19.5	0.5 0.5 0.5	2.0 2.0 2.0	still denser haze	2.720 3.625 2.720	
_	Wetting Concent		0.0914		Average	2.720	* .

*Sandopan DTC Linear Gel 6445-121-5 **Xylene

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Bottle Number	Water	Organic**	Agent'	ŧ	Concentrat	tion _1
	<u>(ml)</u>	<u>(ml)</u>	(grams	3)	(grams/cc)	<u>X 1</u> 0 '
210A 210B 210C	*** 19 19 19	1 1 . 1	0 0 0	Clear with two layers	1.70	
Wetting Concent		0.0000		Average	1.76	
211A 211B 211C	19 19 19	1 1 1	0.5 0.5 0.5	cloudy white with white residue on bottom	1.63 1.61 1.72	
Wetting Concent		0.0237		Average	1.65	
212A 212B 212C	19 19 19	1 1 1	1.0 1.0 1.0	less cloudy white residue on bottom	2.54 2.31 2.24	•
Wetting Concent		0.0462	. •	Average	2.36	
213A 213B 213C	19 19 19	1 1 1	2.0 2.0 2.0	hazytrace of white residue on bottom	2.96 2.68 2.64	•
Wetting Concent	g Agent tration	0.0884		Average	2.76	
214A 214B 214C	19 19 19	1 1 1	4.0 4.0 4.0	hazytrace of white residue on bottom	2.41 2.36	
	g Ågent tration	0.1624		Average	2.38	

*Sandopan DTC Gel Paste **CCl₄

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Bottle Number		Organic** <u>(ml)</u>	Wetting Agent* (grams)		Organic Vapor Concentration (grams/cc) X 10-4	4
215A 215B 215C	*** 19.5 19.5 19.5	0.5 0.5 0.5	0 0 0	clear with two layers	1.33 1.28 1.20	
	Ing Agent entration	0,0000		Average	• 1.27	
216A 216B 216C	19.5 19.5 19.5	0.5	0.5	cloudy white with white residue on bottom	2.04 2.15	
	ing Agent entration	0.0240		Average	2.09	· .
217A 217B 217C		0.5	1.0 1.0 1.0	one clear layer with white residue on bottom	2.07 2.17	
	ing Agent entration	0.0469		Average	2.12	
218A 218B 218C	19.5	0.5 0.5 0.5	2.0 2.0 2.0	one clear layer-trace of residue on bottom	2.60 2.27	
	ing Agent entration	0.0896	:	Average	2.44	
219A 219B 219C	19.5	0.5 0.5 0.5	4.0 4.0 4.0	one clear layer no residue	1.76 2.08	
	ing Agent entration	0.1645		Average	1.92	

*Sandopan DTC Gel Paste ** CCl₄

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TABLE 105

Bottle Number	Water (ml)	Organic** (ml)	Wetting Agent* (grams)	Appearance	Organic Vapor Concentration (grams/cc)X 10-4	
220A 220B 220C	** 19 19 19	1 1 1	0 0 0	two clear layers	2.16	
Wettin Concen	g Agent tration	0.0000		Average	2.10	
221A 221B 221C	19 19 19	1 1 1	0.5 0.5 0.5	one clear layer-white residue on bottom	0.833 1.03	•
	g Agent tration	0.0237		Average	0.93	
222A 222B 222C	19 19 19	1	1.0 1.0 1.0	same as 221	1.81 1.42	
	g Agent tration	0.0462		Average	1.62	
223A 223B 223C	19 19 19	1 1 1	2.0 2.0 2.0	same as 221	1.67 1.74	
	g Agent tration	0.0884		Average	1.71	
224A 224B 224C	19 19 • 19	1 1 1	4.0 4.0 4.0	same as 221	2.54 2.09	*
	gAgent tration	0.1624		Average	2.32	

*Ultrawet 1565 (45.DS) **CCl₄

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TABLE	1	05
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Bottle Number	Water (ml)	Organic** <u>(ml)</u>	Wetting Agent* (grams)	Appearance	Organic Concenti (grams/c	cation
225A 225B 225C	19.5 19.5 19.5	0.5 0.5 0.5	0 0 0	two clear layers	1.46	
	g Agent tration	0.0000		Average	1.55	
226A 226B 226C	19.5 19.5 19.5	0.5 0.5 0.5	0.5 0.5 0.5	one clear layer/white residue on bottom	0.925 1.26 	
Wettin Concen	g Agent tration	0.0240	· .	Average	1.09	•
227A 227B 227C	19.5 19.5 19.5	0.5 0.5 0.5	1.0 1.0 1.0	same as 226	1.48 1.39	
	g Agent tration	0.0469		Average	1.44	
228A 228B 228C	19.5 19.5 19.5	0.5 0.5 0.5	2.0 2.0 2.0	same as 226	1.62 1.57	•
	g Agent tration	0.0896		Average	1.60	
229A 229B 229C	19.5 19.5 19.5	0.5 0.5 0.5	4.0 4.0 4.0	same as 226	2.68 1.99 1.02	
	g Agent tration	0.1645		Average	1.89	• . • .

Bottle Number	Water (ml)	Organic** (ml)	Wetting Agent* (grams)	Appearance	Organic Vapor Concentration (grams/cc)X10-4	
230A 230B 230C	** 19 19 19	1 1 1	0 0 0	two clear layers	1.57 2.16	
	g Agent tration	0.0000		Average	1.87	
231A 231B 231C	19 19 19	1 1 1	0.5 0.5 0.5	two clear layers/white residue on bottom	1.79 1.99	
	g Agent tration	0.0237		Average	1.89	
232A 232B 232C	19 19 19	1 1 1	1.0 1.0 1.0	same as 231	1.70 1.81	
	g Agent tration	0.0462		Average	1.76	:
233A 233B 233C	19 19 19	1 1 1	2.0 2.0 2.0	same as 231.	1.32 1.57 1.89	
	g Agent tration	0.0884		Average .	1.57	
234A 234B 234C	19 19 19	1 1 1	4.0 4.0 4.0	two clear layers	1.63 1.48 1.33	•
	g Agent tration	0.1624		Average	1.48	

*40SX-Lot#5212 **CC1₄

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Bottle Number	Water (ml)	Organic** (ml)	Wetting Agent* (grams)	Appearance	Organic Vapor Concentration (grams/cc) X 10-4
235A 235B 235C	19.5 19.5 19.5	0.5 0.5 0.5	0 0 0	two clear layers	1.76 1.71
Wetting Concent		0.0000		Average	1.74
236A 236B 2360	19.5 19.5 19.5	0.5 0.5 0.5	0.5 0.5 0.5	two clear layers/white residue on bottom	1.07 1.74 1.39
Wetting Concent		0.0240	-	Average	1.40
237A 237B 237C	19.5 19.5 19.5	0.5 0.5 0.5	1.0 1.0 1.0	same as 236	1.46 1.50
Wetting Concent		0.0469		Average	1.48
238A 238B 238C	19.5 19.5 19.5	0.5 0.5 0.5	2.0 2.0 2.0	two clear layers	0.944 1.67 1.33
	g Agent tration	0.0896		Average	1.31
239A 239B 239C	19.5 19.5 19.5	0.5 0.5 Ø.5	4.0 4.0 4.0	same as 238	1.63 1.54 1.46
	g Agent tration	0.1645		Average	1.54
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*40SX-Lot#5212 **CCl₄

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	Bottle Number	Water (ml)	Organic** (ml)	Wetting Agent* (grams)	Appearance	Organic Vapor Concentration (grams/cc)X 10-4
	240A 240B 240C	^{***} 19 19 19	1 1 1	0 0 0	two clear layers	1.85 1.94 2.13
	Wetting Concent		0.0000		Average	1.97
	241A 241B 241C	19 19 19	1 1	0.5 0.5 0.5	white cloudy w/white residue on bottom	z.2.71 2.64
	Wetting		0.0237		Average	2.67
	242A 242B 242C	19 19 19	1 1 1	1.0 1.0 1.0	less cloudy w/ white residue on bottom	3.24 3.05 3.19
	Wetting Concent		0.0462		Average	3.16
	243A 243B 243C	19 19 19	1 1 1	2.0 2.0 2.0	solution hazy-trace whiteresidue on bottom	2.97 3.15
	Wetting Concent	g Agent tration	0.0884		Average	3.06
	244A 244B 244C	19 19 19	1 1 1	4.0 4.0 4.0	same as 243	2.45 2.93
•		g Agent tration	0.1624		Average	2.69
	X(1 - 7 -					

*Sandopan DTC Linear Gel **CCl₄

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TABLE 107

Bottle Number	Water	Organic** <u>(ml)</u>	Wetting Agent* (grams	· · · ·	Organic Vapor Concentration (grams/cc)x 10 ⁻⁴
245A 245B 245C	19.5 19.5 19.5	0.5 0.5 0.5	0 0 0	two clear layers	2.27
Wetting Concent		0.0000		Average	2.32
246A 2 246B 246C	19.5 19.5 19.5	0.5 0.5 0.5	0.5 0.5 0.5	cloudy white-white residue on bottom	2.64 2.51
Wetting Concent		0.0240	•	Average	2.57
247A 247B 247C	19.5 19.5 19.5	0.5 0.5 0.5	1.0 1.0 1.0	one clear layer-white residue on bottom	2.60 2.66
Wetting Concent	g Agent tration	0.0469		Average	2.63
248A 248B 248C	19.5 19.5 19.5	0.5 0.5 0.5	2.0 2.0 2.0	one clear layer-trace white residue on bottom	2.71 2.62 2.76
	g Agent tration	0.0896		Average	2.69
249A 249B 249C	19.5 19.5 19.5	0.5 0.5 0.5	4.0 4.0 4.0	one clear layer no residue	2.31 2.40 2.52
	g Agent tration	0.1645	·	Average	2.41

*Sandopan DTC Linear Gel **CCl₄

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Bottle Number	Water	Organic** <u>(ml)</u>	Wetting Agent* (grams)	Appearance	Organic V Concentra (grams/co	ation _
111A 111B 111C	⁵⁴ 19 19 19	1 1 1	0 0 0	two clear layers	6.56 6.25	
Wetting Concent		0.0000		Average	6.40	
112A 112B 112C	19 19 19	1 1 1	0.5 0.5 0.5	hazy solution	6.61 7.04	
Wetting Concent		0.0246		Average	6.83	
113A 113B 113C	19 19 19	1 1 1	1.0 1.0 1.0	hazy solution	6.68 6.68	•
Wetting Concent		0.0479		Average	6.68	
114A 114B 114C	19 19 19	1 1 1	2.0 2.0 2.0	denser haze	5.26 3.76 2.61	
Wetting Concent		0,0915		Average	3.88	

*Sandopan DTC Gel Paste **Toluene

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TABLE 108

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	Bottle Number	Water (ml)	Organic** (ml)	Wetting Agent* (grams)	Appearance	Organic Vapor Concentration (grams/cc) <u>X</u> 10 ⁻⁵
	115A 115B 115C	^{•••} 19.5 19.5 19.5	0.5 0.5 0.5	0 0 0	two clear layers	6.35 5.22
	Wetting Concent		0.0000	•	Average	5.78
	116A 116B 116C	19.5 19.5 19.5	0.5 0.5 0.5	0.5 0.5 0.5	hazy solution	6.01 5.41
	Wetting Concent		0.0244		Average	5.71
	117A 117B 117C	19.5 19.5 19.5	0.5 0.5 0.5	1.0 1.0 1.0	haz y solution	4.79 5.38
	Wettin _e Concent		0.0486	,	Average	5.09
	118A 118B 118C	19.5 19.5 19.5	0.5 0.5 0.5	2.0 2.0 2.0	denser haze	4.91 4.60
*** **	Wétțing Concent	g Agent tration	0.0912		Average	4.75

*Sandopan DTC Gel Paste **Toluene

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TABLE 109

Bottle Number	Water	Organic**	Wetting Agent* (grams)	Appearance	Organic Vapor Concentration (grams/cc) X 1
429			(BI duits)		
121A 121B 121C	** 19 19 19	1 1 1	0 0 0	two clear layers	7.77 8.14 8.14
	g Agent tration	0.0000		Average	8.02
122A 122B 122C	19 19 19	1 1	0.5 0.5 0.5	hazy solution	8.11 8.25 8.25
	g Agent tration	0.0246		Average	8.20
123A 123B 1230	19 19 19	1 1 1	1.0 1.0 1.0	hazy solution	8.86
	ng Agent Atration	0.0479		Average	8,98
124A 124B 124C	19 19 19	1 1 1	2.0 2.0 2,0	denser haze	9.24 9.69
	ng Agent Atration	0.0915		Average	9.47

*Ultrawet 1565 (45.DS) **Toluene

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Bottle Number	Water	Organic** (ml)	Wetting Agent* (grams)	Appearance	Organic Vapor Concentration (grams/cc)X 10 ⁻⁵
125A 125B 1250	^{**} 19.5 19.5 19.5	0.5 0.5 0.5	0 0 0	two clear layers	9.20 9.37 8.95
Wetting Concent		0.0000		Average	9.17
126A 126B 126C	19.5 19.5 19.5	0.5 0.5 0.5	0.5 0.5 0.5	hazy solution	9.15 9.58
Wetting Concen	g Agent tration	0.0244		Average	9.37
127A 127B 127C	19.5 19.5 19.5	0.5 0.5 0.5	1.0 1.0 1.0	hazy solution	8.86 8.76
Wettin Concen	g Agent tration	0.0486	•	Average	8.81
128A 128B 128C	19.5 19.5 19.5	0.5 0.5 0.5	2.0 2.0 2.0	hazy solution	9.15 9.21
	g Agent tration	0.0912		Average	9.18

Ultrawet 1565 (45.DS) **Toluene

Bottle Number	Water	Organic**	Wetting Agent*	Appearance	Organic Vapor Concentration
MUNDEL	<u>(ml)</u>	<u>(ml)</u>	(grams)		$(grams/cc) \times 10^{-5}$
131A 131B 1310	⁵⁴ 19 19 19	1 1 1	0 0 0	two clear layers	5.65 5.38
	g Agent tration	0.0000		Average	5.52
132A 132B 132C	19 19 19	1 1 1	0.5 0.5 0.5	hazy solution	6.72 6.82
Wettin Concen	g Agent tration	0.0246	•	Average	6.77
133A 133B 133C	19 19 19	1 1 1	1.0 1.0 1.0	hazy solution	6.12 6.04
	g Agent tration	0.0479		Average	6.08
134A 134B 134C	19 19 19	1 1 1	2.0 2.0 2.0	dense r haze	5.60 6.10
Wettin Concen	g Agent tration	0.0915		Average	5.85

*40SX-Lot#5212 **Toluene

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			TABLE	110		
	Bottle Number	Water	Organic**	Wetting Agent*	Appearance	Concentration _
	Påri Gauria, i sup film film	<u>(ml)</u>	<u>(ml)</u>	(grams)		$(grams/cc)\chi_{10}^{-5}$
	135A 135B 135C	19.5 19.5 19.5	0.5 0.5 0.5	0 0 0	two clear layers	5.26 5.38
	Wetting Concentr		0.0000		Average	5.32
	136A 136B 136C	19.5 19.5 19.5	0.5 0.5 0.5	0.5 0.5 0.5	hazy solution	3.35 3.64
	Wetting Concentr		0.0244		Average	3.50
	137A 137B 137C	19.5 19.5 19.5	0.5 0.5 0.5	1.0 1.0 1.0	hazy solution	4.69 5.69
• ΄ :	Wetting Concent		0.0486		Average	5.19
	138A 138B 138C	19.5 19.5 19.5	0.5 0.5 0.5	2.0 2.0 2.0	denser haze	4.11 4.19
	Wetting Concent:		0.0912		Average	4.15

*40SX-Lot#5212 **Toluene

	ottle umber	Water (ml)	Organic** <u>(ml)</u>	Wetting Agent* (grams)	Appearance	Organic Vapor Concentration (grams/cc)X 10-5
	141A 141B 141C	⁵⁴ 19 19 19	1 1 1	0 0 0	two clear layers	6.10 6.10
	Wetting Concent		0.0000		Average	6.10
	142A 142B 142C	19 19 19	1 1 1	0.5 0.5 0.5	hazy solution	3.88 5.29 6.82
-	Wetting Concent		0.0246		Average	5.33
	143A 143B 1430	19 19 19	1 1 1	1.0 1.0 1.0	hazy solution	<u>6.49</u> 7.40
·	Wetting Concent		0.0479		Average	6.95
	144A 144B 144C	19 19 19	1 1 1	2.0 2.0 2.0	denser haze	3.26 3.71
· · ·	Wetting Concent		0.0915		Average	3.49

*Sandopan DTC Linear Gel **Toluene

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TABLE 111

Bottle Number	Water	Organic**	Agent*	Appearance	Organic Vapor Concentration
	<u>(ml)</u>	<u>(ml)</u>	(grams)		<u>(grams/cc)X 1</u> 0 ⁻⁹
145A 145B 145C	** 19.5 19.5 19.5	0.5 0.5 0.5	0 0 0	two clear layers	6.27 6.25
	ng Agent ntration	0.0000		Average	6.26
146А 146в 146С	19.5 19.5 19.5	0.5 0.5 0.5	0.5 0.5 0.5	hazy solution	7.04 7.11
Wettin Conce	ng Agent ntration	0.0244	:	Average	7.08
147A	19.5	0.5	1.0	hazy	7.04
147B 147C	19.5 19.5	0.5	1.0	solution	7.04
	ng Agent ntration	0.0486		Average	7.04
148A	19.5	0.5	2.0	hazy	2.80
148B 148C	19.5 19.5	0.5 0.5	2.0 2.0	(denser) solution	4.59 6.51
	ng Agent ntration	0.0912	•	Average	4.97

*Sandopan DTC Linear Gel **Toluene

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<i>.</i> ,	Bottle Number	Water (ml)	Organic**	Wetting Agent* (grams)	Appearance	Organic V Concentra (grams/cc	tion
	310A 310B 310C	[™] 19 19 19	1 1 1	0 0 0	one clear layer	5.88 5.94	
	Wetting Concent		0.0000		Average	5.91	
••••	311A 311B 311C	19 19 19	1 1 1	0.5 0.5 0.5	one clear layer	<u>6.17</u> 6.74	
•	Wetting Concent		0.0245	• ·	Average	6.74	
	312A 312B 312C	19 19 19	1 1 1	1.0 1.0 1.0	one clear layer	7.03 7.16	
	Wetting Concent:		0.0478		Average	7.10	
	313A 313B 313C	19 19 19	1 1 1	2.0 2.0 2.0	one clear layer	2.01	
· 	Wetting Concent:	Agent ration	0.0959		Average	2.67	
	314A 314B 314C	19 19 - 19	1 1 1	4.0 4.0 4.0	one clear layer	4.76 4.74	
	Wetting Concent		0.1674		Average	4.75	

*Sandopan DTC Gel Paste **Ethyl Acetate

• •		TABLE	112		
Bottle Number	Water <u>(ml)</u>	Organic** <u>(ml)</u>	Wetting Agent* (grams)	Appearance	Organic Vapor Concentration (grams/cc) X 10 ⁻⁴
315 A 315 B 315 C	^{***} 19.5 19.5 19.5	0.5 0.5 0.5	0 0 0	one clear layer	3.44 2.44 4.71
- Wettin Concen	g Agent tration	0.0000	:	Average	3.53
316A 316B 316C	19.5 19.5 19.5	0.5 0.5 0.5	0.5 0.5 0.5	one clear layer	5.68 4.65 4.04
	g Agent tration	0.0244	•	Average	4.34
317A 317B 317C	19.5 19.5 19.5	0.5 0.5 0.5	1.0 1.0 1.0	one clear layer	5.02 4.91
	ng Agent Atration	0.0477		Average	4.97
318A 318B 318C	19.5 19.5 19.5	0.5 0.5 0.5	2.0 2.0 2.0	one clear layer	2.72
	ng Agent Atration	0.0911		Average	2.72
319A 319B 319C	19.5 19.5 19.5	0.5 0.5 0.5	4.0 4.0 4.0	one clear layer	5.85 4.39
Wettir Concer	ng Agent ntration	0.1670		Average	5.12

*Sandopan DTC Gel Paste **Ethyl Acetate

TABLE 113

	Bottle Number	Water (ml)	Organic**	Wetting Agent* (grams)	Appearance	Organic Vapor Concentration (grams/cc)X_10 ⁻⁴
. '	320A 320B 320C	** 19 19 19	1 1 1	0 0 0	one clear layer	12.6 12.2
	Wetting Concent:	Agent ration	0.0000		Average	12.4
	321A 321B 3210	19 19 19	1	0.5 0.5 0.5	one clear layer	9.45 9.76
	Wetting Concent		0.0245	•	Average	9.60
	322A 322B 322C	19 19 19	. 1 1 1	1.0 1.0 1.0	one clear layer	8.22 7.02
	Wetting Concent	Agent ration	0.0478	• • • •	Average	7.62
	323A 323B 3230	19 19 19	1 1 1	2.0 2.0 2.0	one clear layer	8.45 8.05
-	Wetting Concent		0.0959		Average	8.25
·	324A 324B 324C	19 19 19	1 1 1	4.0 4.0 4.0	one clear layer	7.02 7.16
	Wetting Concent *Ultraw **Ethyl	ration et 1565 (4	0.1674 15.DS)		Average	7.09
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TABLE 113

Bottle Number	Water (ml)	Organic** (<u>ml)</u>	Wetting Agent* <u>(grams)</u>	Appearance	Organic Vapor Concentration (grams/cc)X 10-4
325 A 325B 325C	19.5 19.5 19.5	0.5 0.5 0.5	0 0 0	one clear layer	5.01 5.33
Wetting Concent		0.0000		Average	5.17
326A 326B 326C	19.5 19.5 19.5	0.5 0.5 0.5	0.5 0.5 0.5	one clear layer	4.47 <u></u> 4.76
Wetting		0.0244		Average	4.62
327A 327B 3270	19.5 19.5 19.5	0.5 0.5 0.5	1.0 1.0 1.0	one clear layer	5.16 5.30
	g Agent tration	0.0477		Average	5.23
328A 328B 328C	19.5 19.5 19.5	0.5 0.5 0.5	2.0 2.0 2.0	one clear layer	5.12 4.73 5.44
	g Agent tration	0.0911	• •	Average	5.10
329A 329B 329C	19.5 19.5 19.5	0.5 0.5 0.5	4.0 4.0 4.0	one clear layer	2.44 3.29
	g Agent tration	0.1670		Average	2.86

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*Ultrawet 1565 (45.DS) **Ethyl Acetate

TABLE 114

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Bottle Number	Water	Organic** (ml)	Wetting Agent* (grams)	Appearance	Organic Vapo Concentratio (grams/cc) X	n ,
330A 330B 330C	<u>(ml)</u> ™ 19 19 19	1 1 1	0 0 0	one clear layer	<u>10.1</u> 10.3	_10
Wetting Cøncent	g Agent cration	0.0000	•	Average	10.2	
331A 331B 331C	19 19 19	1 1 1	0.5 0.5 0.5	one clear layer	12.8 13.1 13.8	
Wetting Concent		0.0245	• • •	Average	13.2	•
332A 332B 332C	19 19 19	1 1 1	1.0 1.0 1.0	one clear layer	12.1 12.9	
Wetting	g Agent tration	0.0478		Average	12.5	
333A 333B 333C	19 19 19	1 1 1	2.0 2.0 2.0	one clear layer	12.8 12.6	 •
	g Agent tration	0.0959		Average	12.7	
334A 334B 334C	19 19 19	1 1 1	4.0 4.0 4.0	one clear layer	10.4 9.85	
Wetting Concent	g Agent tration	0.1674		Average	10.1	
*40SX-1	Lot#5212					

*40SX-Lot#5212 **Ethyl Acetate

TABLE 114

Bottle Number	Water	Organic**	Agent*	Appearance	Concent	ration
	<u>(ml)</u>	<u>(ml)</u>	(grams)			<u>'cc) X 1</u> (
335A	··· 19.5	0.5	0	one	7.80	
335B 3350	19.5 19.5	0.5 0.5	0	clear layer	7.34	
	g Agent tration	0.0000	·	Average	7.57	
336A	19.5	0.5	0.5	one	5.17	
336B	19.5	0.5	0.5	clear	5.14	
3360	19.5	0.5	0.5	layer		
Wettin Concen	g Agent tration	0.0244	-	Average	5.16	···· .
337A	19.5	0.5	1.0	one		
337B	19.5	0.5	1.0	clear	6.05	
3370	19.5	0.5	1.0	layer	5.44	
Wettin	g Agent		· · · ·			
Concen	tration	0.0477	· · ·	Average	5.74	
338A	19.5	0.5	2.0	one	5.44	
338B 3380	19.5 19.5	0.5 0.5	2.0 2.0	clear layer	4.70	
Wettin	g Agent	0.0911		Average	5.07	•
339A	19.5	0.5	4.0	one		
3 39B	19.5	0.5	4.0	clear	4.47	
3390	19.5	0.5	4.0	layer	4.56	·
Wettin	g Agent	. '				
	tration	0.1670		Average	4.52	

*40SX-Lot#5212 **Ethyl Acetate

TABLE 115

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	ottle umber	Water (ml)	Organic**	Wetting Agent* (grams)	Appearance	Organic Vapor Concentration (grams/cc) X_10 ⁻⁴
	340A 340B 340C	** 19 19 19	1 1 1	0 0 0	one clear layer	11.9 11.5
	Wettin Concen	g Agent tration	0.0000		Average	11.7
	341A 341B 341C	19 19 19	1 1 1	0.5 0.5 0.5	one clear layer	11.9 11.2 10.9
•	Wettin Concen	g Agent tration	0.0245		Average	11.4
	342A 342B 342C	19 19 19	1 1 1	1.0 1.0 1.0	one clear layer	10.4 9.80
		ng Agent Atration	0.0478		Average	10.1
	343A 343B 343C	19 19 19	1 1 1	2.0 2.0 2.0	one clear layer	9.74 9.74
-		ng Agent ntration	0.0959		Average	9.74
	344A 344B 344C	19 19 · 19	1 1 1	4.0 4.0 4.0	one clear layer	9.91 9.31
•	Wettin Concer	ng Agent ntration	0.1674		Average	9.61

*Sandopan DTC Linear Gel **Ethyl Acetate

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		TABLE	115			
Bottl Numbe		Organic**	Wetting Agent*	Appearance	Organic Concent:	
	<u>(ml)</u>	<u>(ml)</u>	(grams)		(grams/	
345A 345B 345C	*** 19.5 19.5 19.5	0.5 0.5 0.5	0 0 0	one clear layer	6.76 6.67	
Wett: Conce	ing Agent entration	0.0000	·	Average	6.62	
346A 346B 3460	19.5	0.5 0.5 0.5	0.5 0.5 0.5	one clear layer	.4.44 6.19 5.27	
	ing Agent entration	0.0244		Average	5.30	· · · ·
347A 347B 347C	19.5	0.5 0.5 0.5	1.0 1.0 1.0	one clear layer	5.36 5.16 5.16	· ·
	ing Agent entration	0.0477		Average	5.23	
348A 348B 348C	19.5	0.5 0.5 0.5	2.0 2.0 2.0	one clear layer	5.74 5.54	
	ing Agent entration	0.0911		Average	5.64	
349A 349B 349C		0.5 0.5 0.5	4.0 4.0 4.0	one clear layer	3.58 3.58	
Wett Conc	ing Agent entration	0.1670		Average	3.58	

*Sandopan DTC Linear Gel **Ethyl Acetate

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	•		TABLE	116			
	Bottle Number	Water	Organic** (ml)	Wetting Agent* (grams)	Appearance	Organic V Concentra (grams/cc	tion _6
-	<u></u>	<u>(ml)</u>	<u>(m1)</u>	(Brans)		<u>(Brand) 00</u>	<u>/</u> <u>/</u> <u>/</u> ()
	410A 410B 410C	³⁴ 19 19 19 '	1 1 1	0 0 0	one clear layer	3.01 2.90	
	Wetting Concent		0.0000	·	Average	2.95	. •
	411A 411B 411C	19 19 19	1 1 1	0.5 0.5 0.5	one clear layer	2.53 2.48	
	Wetting Concent		0. 0246		Average	2.50	· · ·
	412A 412B 412C	19 19 19	1 1 1	1.0 1.0 4.0	one clear layer	3.01 3.03	
	Wetting Concent		0.0481		Average	3:02	
	413A 413B 413C	19 19 19	1 1 1	2.0 2.0 2.0	one clear layer	1.91 2.88 2.43	•
-	Wetting Concent		0.0918		Average	2.41	
	414A 414B 414C	19 19 19	1 1 1	4.0 4.0 4.0	one clear layer	2.69 2.93	
	Wetting Concent	Agent ration	0.1681		Average	2.81	

*Sandopan DTC Gel Paste **Isopropyl Alcohol

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	Bottle Number	Water	Organic**	Agent*	Appearance	Organic V Concentra (grams/cc	tion
	415A 415B 415C	(m1) 19.5 19.5 19.5	(ml) 0.5 0.5 0.5	(grams) 0 0 0	one clear layer	2.67 4.13	<u>) </u>
	Wetting	- · ·	0.0000		Average	3:23	
:	416A 416B 416C	19.5 19.5 19.5	0.5 0.5 0.5	0.5 0.5 0.5	one clear layer	2.30 4.03	
•	Wetting Concen	g Agent tration	0.0245	.	Average	3.16	
	417A 417B 417C	19.5 19.5 19.5	0.5 0.5 0.5	1.0 1.0 1.0	one clear layer	0.392 0.392	
		g Agent tration	0.0479		Average	0.392	
•	418A 418B 418C	19.5 19.5 19.5	0.5 0.5 0.5	2.0 2.0 2.0	one cl e ar layer	1.52 1.52	
		g Agent tration	0.0914		Average	1.52	• • •
	419A 419B 419C	19.5 19.5 - 19.5	0.5 0.5 0.5	4.0 4.0 4.0	one elear layer	0.549	
		g Agent tration	0.1676		Average	0.471	
	· ·	. •		· ·			

*Sandopan DTC Gel Paste **Isopropyl Alcohol

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TABLE 117

	Bottle Number	Water (ml)	Organic** (ml)	Wetting Agent* (grams)	Appearance	Organic Vapor Concentration (grams/cc)X 10-6
	420A 420B 420C	*** 19 19 19	1 1 1	0 0 0	one clear layer	2.56 3.14
	Wetting Concent	Agent ration	0.0000	•	Average	2.85
	421A 421B 421C	19 19 19	1 1 1	0.5 0.5 0.5	one clear layer	2.82
•	Wetting Concent		0.0246		Average	2.51
	422A 422B 422C	19 19 19	1 1 1	1.0 1.0 1.0	one clear layer	3.03 3.06 3.24
	Wetting Concent		0.0481		Average	3.11
	423A 423B 423C	19 19 19	1 1 1	2.0 2.0 2.0	one clear layer	3.40 <u></u> 3.14
-	Wetting Concent	; Agent cration	0.0918		Average	3.27
	424A 424B 424C	19 19 19	1 1 1	4.0 4.0 4.0	one clear layer	2.80 2.56 2.51
•	Wetting Concent		0.1681		Average	2.63

*Ultrawet 1565 (45.DS) **Isopropyl Alcohol

TABLE 117

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	Bottle Number	Water	Organic**	Wetting Agent*	Appearance	Organic Vapor Concentration
-		<u>(ml)</u>	<u>(ml)</u>	(grams)		$(grams/cc) \times 10^{-6}$
-	425A 425B 425C	19.5 19.5 19.5	0.5 0.5 0.5	0 0 0	one clear layer	1.25 1.96
•	Wetting Concent		0.0000	•	Average	1.60
	426A 426B 426C	19.5 19.5 19.5	0.5 0.5 0.5	0.5 0.5 0.5	one clear layer	0.968
	Wetting Concent	g Agent tration	0.0245		Average	0.798
	427A 427B 427C	19.5 19.5 19.5	0.5 0.5 0.5	1.0 1.0 1.0	one clear layer	1.25 1.10
	Wetting Concent	g Agent tration	0.0479	· · · · · · · · · · · · · · · · · · ·	Average	1.17
	428A 428B 428C	19.5 19.5 19.5	0.5 0.5 0.5	2.0 2.0 2.0	one clear layer	1.20 1.57
		g Agent tration	0.0914		Average	1.39
. •	429A 429B 429C	19.5 19.5 19.5	0.5 0.5 0.5	4.0 4.0 4.0	one clear layer	0.870 0.870
		g Agent tration	0.1676		Average	0.870
			•		•	

*Ultrawet 1565 (45.DS) **Isopropyl Alcohol

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TABLE 118

	Bottle Number	Water	Organic**	Agent*	Appearance	Concentra	ation _6
		<u>(ml)</u>	<u>(ml)</u>	(grams)		(grams/co	<u>c)X 10</u> °
	435A 435B 435C	*** 19.5 19.5 19.5	0.5 0.5 0.5	0 0 0	one clear layer	0.392 0.601	
	Wetting Concent		0.0000		Average	0.497	
	436A	19.5	0.5	0.5	one	0.471	
	436B 4360	19.5 19.5	0.5	0.5 0.5	clear layer	0.523	. 1
•	Wetting Concent		0.0245	• •	Average	.0.497	
	437A	19.5	0.5	1.0	one		
	437B 437C	19.5 1 <u>9</u> .5	0.5	1.0	clear layer	های مید منت منت مید اند مید اند مید	
	Wetting Concent		0.0479		Average		
	438A	19.5	0.5	2.0	one		
	438B 4380	19.5. 19.5	0.5	2.0	clear layer	1.10 0.836	
	Wetting		A A A A A		-		
	Concent	ration	0.0914		Average	0.936	
	439A 439B	19.5 19.5	0.5	4.0 4.0	one clear	0.942	.
	439C	19.5	0.5	4.0	layer		
	Wetting		0 1676	•		0.040	· . ·
	Concent	ration	0.1676		Average	0.942	

*40SX-Lot#5212 **Isopropyl Alcohol

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TABLE 118

Bottle Number	Water (ml)	Organic**	Wetting Agent* (grams)	Appearance	Organic Vapor Concentration (grams/cc)X_10-6
430A 430B 430C	19 19 19 19	1 1 1	0 0 0	one clear layer	3.01 3.40
Wetting Concen	g Agent tration	0.0000	• • •	Average	3.20
431A 431B 431C	19 19 19	1 1 1	0.5 0.5 0.5	one clear layer	2.48
Wettin Concen	g Agent tration	0.0246		Average	2.44
432A 432B 432C	19 19 19	1 1 1	1.0 1.0 1.0	one clear layer	3.27 2.75
	g Agent tration	0.0481		Average	3.01
433A 433B 433C	19 19 - 19	1 1 1	2.0 2.0 2.0	one clear layer	2.43 2.48
	g Agent tration	0.0918		Average	2.45
434A 434B 434C	19 19 19	1 1 1	4.0 4.0 4.0	one clear layer	2.75 2.88
	g Agent tration	0.1681		Average	2.82

*40SX-Lot#5212 **Isopropyl Alcohol

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Bottle Number	Water	Organic** (ml)	Wetting Agent* (grams)	Appearance	Organic Vapor Concentration (grams/cc) X 10
440A 440B 440C	²⁴ 19 19 19	1 1 1	0 0 0	one clear layer	3.35 2.67
	g Agent tration	0.0000	• •	Average	3.01
441A 441B 441C	19 19 19	1 1 1	0.5 0.5 0.5	one clear layer	1.44 2.33 0.916
Wettin Concen	g Agent tration	0.0246	•	Average	1.56
442A 442B 442C	19 19 19	1 1 1	1.0 1.0 1.0	one clear layer	2.69 1.44 4.29
	g Agent tration	0.0481		Average	2.81
443A 443B 443C	19 19 19	1 1 1	2.0 2.0 2.0	one clear layer	1.83 2.17
	g Agent tration	0.0918		Average	2.00
444A 444B 444C	19 19 19	1 1 1	4.0 4.0 4.0	one clear layer	3.92 1.20
	g Agent tration	0.1681		Average	2.56

*Sandopan DTC Linear Gel **Isopropyl Alcohol

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	ottle umber	Water	Organic**	Wetting Agent*	Appearance	Organic Va Concentrat	ion_6
-		<u>(ml)</u>	<u>(ml)</u>	(grams)		(grams/cc))	<u>(1</u> 0 °
•	445A 445B 4450	19.5 19.5 19.5	0.5 0.5 0.5	0 0 0	one clear layer	1.88 2.04 1.83	
		g Agent tration	0.0000	·	Average	1.92	
• •	446A 446B 446C	19.5 19.5 19.5	0.5 0.5 0.5	0.5 0.5 0.5	one clear layer	2.20 2.20	
•		g Agent tration	0.0245	•	Average	2.20	
	447A 447B 447C	19.5 19.5 19.5	0.5 0.5 0.5	1.0 1.0 1.0	one clear layer	 1.83	
		ng Agent Atration	0.0479	•	Average	1.83	
<i>,</i>	448A 448B 448C	19.5 19.5 19.5	0.5 0.5 0.5	2.0 2.0 2.0	one clear layer	0.968 0.942	
		ng Agent Atration	0.0914		Average	0.955	
	449A 449B 449C	19.5 19.5 19.5	0.5 0.5 0.5	4.0 4.0 4.0	one clear layer	2.77	
		ng Agent Atration	0.1676		Average	2.72	
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*Sandopan DTC Linear Gel **Isopropyl Alcohol

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Bottle Number	Water	Organic**	Wetting Agent*	Appearance	Organic Vapor Concentration
	<u>(ml)</u>	<u>(ml)</u>	(grams)	and the state of the second	(grams/cc) X 10-6
OAOA OAOB OAOC	*** 19 19 19	1 1 1	0 0 0	clear with small xylene bubbles	6.83 7.90
Wetting Concent	g Agent tration	0.0000		Average	7.37
OA1A OA1B OA1C	19 19 19	1 1 1	0.5 0.5 0.5	hazy with white residue on top	10.7 14.4
Wetting Concent	g Agent tration	0.0245	• •.	Average	12.6
OA2A OA2B OA2C	19 19 19	1 1 1	1.0 1.0 1.0	hazy with white residue on top	11.1 10.3
Wetting Concen	g Agent tration	0.0478	•	Average	10.7
0A3A 0A3B 0A3C	19 19 19	1 1 1	2.0 2.0 2.0	clear sol. w/ white residue on top	10.8 10.7 11.5
Wetting Concen	g Agent tration	0.0913		Average	11.0
0A4A 0A4B 0A4C	19 19 19	1 1 1	4.0 4.0 4.0	clear sol. yellowish trace white residue	10.7 13.6
	g Agent tration	0.1673		Average	12.2

*Stepanol WAT **Xylene

Bottle Number	Water	Organic** (ml)	Wetting Agent* (grams)		Organic Vapor Concentration (grams/cc) X 10 ⁻⁶
0A5A 0A5B 0A5C	**************************************	0.5 0.5 0.5	0 0 0	clear sol. w/ xylene bubbles	11.8 12.6
Wetting Concent		0.0000	•	Average	12.2
0A6A 0A6B 0A6C	19.5 19.5 19.5	0.5 0.5 0.5	0.5 0.5 0.5	clear sol. traces white residue on top	<u>13.5</u> <u>12.6</u>
Wetting Concemt:		0.0244		Average	13.1
0A7A 0A7 <u>B</u> 0A7C	19.5 19.5 19.5	0.5 0.5 0.5	1.0 1.0 1.0	clear sol. less residue than OA6	11.5 9.05
Wetting Concent		0.0477	•	Average	10.3
OA8A OA8B OA8C	19.5 19.5 19.5	0.5 0.5 0.5	2.0 2.0 2.0	clear sol. see OA7	13.4 14.2
Wetting Concemt		0.0911		Average	13.8
0A9A 0A9B 0A9C	19.5 19.5 19.5	0.5 0.5 0.5	4.0 4.0 4.0	yellowish clear sol. white residue on top	11.9 14.5
Wetting Concent		0.1670		Average	12.9

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*Stepanol WAT **Xylene

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Bottle Number	Water (ml)	Organic** <u>(ml)</u>	Wetting Agent* (grams)	Appearance	Organic Vapor Concentration (grams/cc) <u>x 1</u> 0 ⁻⁶
OBOA OBOB OBOC	19 19 19	1 1 1	0 0 0	clear solution	4.28
Wetting Concent		0.0000	• 7 • •	Average	4.40
0B1A 0B1B 0B10	19 19 19	1 1 1	0.5 0.5 0.5	milky white solution	8.06 6.83
Wetting Concent	g Agent cration	0.0245	••• • • • •	Average	7.44
OB2A OB2B OB2C	19 19 19	1 1 1	1.0 1.0 1.0	milky white solution	4.28 6.09
Wetting Concent		0.0478	· · ·	Average	5.18
OB3A OB3B OB3C	19 19 19	1 1 1	2.0 2.0 2.0	milky white solution	6.91 4.94
Wetting Concent	g Agent tration	0.0913		Average	5.92
OB4A OB4B OB4C	19 19 19	1 1 1	4.0 4.0 4.0	milky white solution	3.87 8.81 5.76
	g Agent. tration	0.1673	. · ·	Average	6.14
	. *				

*Steol KS-460 **Xylene

TABLE 121

Bottle	Water	Organic**		Appearance	Organic Vapor Concentration
Number	<u>(ml)</u>	<u>(ml)</u>	Agent* (grams)		(grams/cc) X 10
0B5A 0B5B 0B5C	19.5 19.5 19.5	0.5 0.5 0.5	0 0 0	clear solution	6.17 5.51
Wetting Concent	g Agent tration	0.0000		Average	5.84
0B6A 0B6B 0B6C	19.5 19.5 19.5	0.5 0.5 0.5	0.5 0.5 0.5	milky white solution	7.32 6.42
	g Agent tration	0.0244	· · ·	Average	6.87
0B7A 0B7B 0B7C	19.5 19.5 19.5	0.5 0.5 0.5	1.0 1.0 1.0	milky white	11.8 10.0
Wetting Concen	g Agent tration	0.0477	•	Average	10.9
OB8A OB8B OB8C	19.5 19.5 19.5	0.5 0.5 0.5	2.0 2.0 2.0	milky white	8.81 7.74
	g Agent tration	0.0911		Average	8.27
0B9A 0B9B ÒB 9C	19.5 19.5 19.5	0.5 0.5 0.5	4.0 4.0 4.0	clear solution	10.7 9.14 11.5
	g Agent tration	0.1670		Average	10.4
*Steol	KS - 460			- - -	

*Steol KS-460 **Xylene

	Bottle Number	Water (ml)	Organic* <u>(ml)</u>	* Wetting Agent* (grams)	Appearance	Organic Vapor Concentration (grams/cc) <u>X 1</u> 0-6
•	OCOA OCOB OCOC	19 19 19	1 1 1	0 0 0	clear sol. w/ xylene bubbles	8.31 10.6 9.21
	Wetting Concent	g Agent cration	0.0000	•	Average	9.37
•	001A 001B 0010	19 19 19	1 1 1	0.5 0.5 0.5	hazy sol. w/ white residue	9.87 8.64 11.8
		g Agent tration	0.0245	•	Average	10.1
	OC2A OC2B OC2C	19 19 19	1 1 1	1.0 1.0 1.0	hazy sol. w/ white residue	9.87 8.64 11.5
•	Wetting Concent	g Agent tration	0.0478	; ;	Average	10.0
·	003A 003B 0030	19 19 19	1 1 1	2.0 2.0 2.0	milky yellow solution	9.13 12.6 7.07
	Wetting Concen	g Agent tration	0.0913)	Average	8.10
	0C4A 0C4B 0C4C	19 19 19	1 1 1	4.0 4.0 4.0	thick yellow gel	10.5 10.2
		g Agent tration	0.1673	3	Average	10.4
	*N1 ~~ ~ 7	1001	·.			

*Ninol 1281 **Xylene

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TABLE 122

Bottle	Water	Organic**	-	Appearance	Organic Vapor Concentration
Number	<u>(ml)</u>	<u>(ml)</u>	Agent* <u>(grams)</u>		$(grams/cc) \times 10^{-6}$
005A 005B 0050	19.5 19.5 19.5	0.5 0.5 0.5	0 0 0	clear sol. w/ xylene bubbles	8.64 5.59 10.3
	g Agent tration	0.0000	• •	Average	7.11
006A 006B 0060	19.5 19.5 19.5	0.5 0.5 0.5	0.5	hazy sol. w/ white residue	7.57 7.81 7.90
	g Agent tration	0.0244	•	Average	7.76
0C7A 0C7B 0C7C	19.5 19.5 19.5	0.5 0.5 0.5	1.0 1.0 1.0	hazy sol. w/ yellow tinge	6.66 6.83
	g Agent tration	0.0477	•	Average	6.74
008A 008B 008C	19.5 19.5 19.5	0.5 0.5 0.5	2.0 2.0 2.0	milky yellow solution	8.23 8.23
	g Agent tration	0.0911		Average	8.23
009A 009B 0090	19.5 19.5 19.5	0.5 0.5 0.5	4.0 4.0 4.0	thick yellow gel	7.24 9.05 8.23
	g Agent tration	0.1670	· ·	Average	8.17
·				•	

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*Ninol 1281 **Xylene

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TABLE 123

: •	Bottle Number	Water <u>(ml)</u>	Orga <u>(ml)</u>	nic**	Wetting Agent* (grams)	Appearance	Organic Vapor Concentration (grams/cc) X_10 ⁻⁶
	ODOA ODOB ODOC	19 19 19	1 1 1	· .	0 0 0	clear sol. w/ xylene bubbles	8.23 12.0
	Wettin Concen	g Agent tration	0.	0000		Average	10.7
•	OD1A OD1B OD1C	19 19 19	1 1 1	•	0.5 0.5 0.5	milky light-gray	 10.6 11.4
		g Agent tration	0	0245		Average	11.0
	OD2A OD2B OD2C	19 19 19	1 ●1 1		1.0 1.0 1.0	milky white	9.46 6.74
		g Agent tration	Ō	.0478		Average	8.10
	OD3A OD3B OD3C	19 19 19	1 1 1		2.0 2.0 2.0	off-white	8.23 9.46
		g Agent tration	0	.0913		Average	8.84
	OD4A OD4B OD4C	19 19 19	1 1 1	•	4.0 4.0 4.0	off-yellow	10.4 10.4
		g Agent tration	0	.1673		Average	10.4
	*Stepa **Xylen	ntex WB42 e	2				

**Xylene . •

TABLE 123 .

	ttle mber	Water	Organic**	Wetting Agent*	Appearance	Organic Vapor Concentration
		<u>(ml)</u>	<u>(ml)</u>	(grams)	and a state while the state of the second state of	$(grams/cc)X_10^{-6}$
0	D5A D5B D5C	** 19.5 19.5 19.5	0.5 0.5 0.5	0 0 0	clear sol. w/ xylene bubbles	12.4 13.2
	etting oncent:		0.0000	· ·	Average	12.8
0	D6A D6B D6C	19.5 19.5 19.5	0.5 0.5 0.5	0.5 0.5 0.5	milky light gray	8.64 8.97
	etting oncent		0.0244		Average	8.80
C	D7A D7B D7C	19.5 19.5 19.5	0.5 0.5 0.5	1.0 1.0 1.0	milky white	-10.6 11.6 10.9
	letting Soncent		0.0477	•	Average	11.0
Ċ	D8A D8B D8C	19.5 19.5 19.5	0.5 0.5 0.5	2.0 2.0 2.0	hazy grayish	10.0 11.0 8.72
		Agent	0.0911		Average	9.90
(DD9A DD9B DD9C	19.5 19.5 19.5	0.5	4.0 4.8	off-yellow transparent	7.16 5.84
	Vetting Concent	Agent Tation	0.1670		Average	6.50
÷	*Stepar	tex WB42			•	
*:	*Xýléne)				

	Bottle Number	Water (ml)	:	Organ <u>(ml)</u>	ic**	Wetting Agent* (grams)	Appearance	Organic Vapor Concentration (grams/cc)X 10-6
	OEOA OEOB OEOC	19 19 19		1 1 1		0 0 0	clear sol. w/ xylene bubbles	9.38 10.2
•	Wetting		·	0.00	000	•	Average	9.79
•	OE1A OE1B OE1C	19 19 19		1 1 1	· · · ·	0.5 0.5 0.5	milky white	8.64 9.54
	Wetting Conce n	g Agent tration		0.0	245		Average	9.09
•	OE2A OE2B OE2C	19 19 19	•	1 1 1		1.0 1.0 1.0	milky white	9.71 8.64
		g Agent tration		0.0	478		Average	9.17
	OE3A OE3B OE3C	19 19 19	·	1 1 1		2.0 2.0 2.0	milky-white yellow tinge	9.79
	Wettin Concen	g Agent tration		0.0	913	· · · · · ·	Average	9.75
	OE4A OE4B OE4C	19 19 19		1 1 1		4.0 4.0 4.0	light yellow translucent solution	5.67 6.91
		g Agent tration		0.1	673		Average	6.29

*Toximul R **Xylene

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(ml) 19.5 19.5	<u>(ml)</u>	Agent* (grams)		Concentration (grams/cc)x 10
19.5				VEL amo/ CC/A 10
19.5	0.5 0.5 0.5	0 0 0	clear sol. w/ xylene bubbles	8.23 8.64 8.39
Agent	0.0000	•	Average	8.42
19.5 19.5 19.5	0.5 0.5 0.5	0.5 0.5 0.5	milky white solution	9.79 8.97
Agent	0.0244		Average	9.38
19.5 19.5 19.5	0.5 0.5 0.5	1.0 1.0 1.0	milky white solution	9.05 9.71
Agent ration	0.0477		Average	9.38
19.5 19.5 19.5	0.5 0.5 0.5	2.0 2.0 2.0	hazy grayish solution	9.05 9.62
Agent ration	0.0911		Average	9.33
19.5 19.5 19.5	0.5 0.5 0.5	4.0 4.0 4.0	clear yellowish solution	7.81 8.64
Agent	0.1670		Average	8.22
		· .		
	ration 19.5 19.5 19.5 Agent ration 19.5 19.5 19.5 Agent ration 19.5 19.5 19.5 19.5 19.5 19.5 Agent ration 19.5 1	ration0.000019.50.510.1670	ration 0.0000 19.5 0.5 0.5 19.5 0.5 0.5 19.5 0.5 0.5 Agent 0.0244 19.5 0.5 1.0 19.5 0.5 1.0 19.5 0.5 1.0 19.5 0.5 1.0 19.5 0.5 1.0 19.5 0.5 1.0 Agent 0.0477 19.5 0.5 2.0 19.5 0.5 2.0 19.5 0.5 2.0 Agent 0.0911 19.5 19.5 0.5 4.0 19.5 0.5 4.0 19.5 0.5 4.0 Agent 0.1670 1 R 0.1670	ration 0.0000 Average 19.5 0.5 0.5 milky 19.5 0.5 0.5 white 19.5 0.5 0.5 solution Agent 0.0244 Average 19.5 0.5 1.0 milky 19.5 0.5 1.0 milky 19.5 0.5 1.0 white 19.5 0.5 1.0 white 19.5 0.5 1.0 white 19.5 0.5 1.0 solution Agent 0.0477 Average 19.5 0.5 2.0 hazy 19.5 0.5 2.0 solution Agent 0.0911 Average 19.5 0.5 4.0 yellowish 19.5 0.5 4.0 solution Agent 0.1670 Average 1 1 R 1 1 Average 1

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Bottle Number	Water (ml)	Organic** <u>(ml)</u>	Wetting Agent* (grams)	Appearance	Organic Vapor Concentration (grams/cc)X 10
OFOA OFOB OFOC	** 19 19 19	1 1 1	0 0 0	clear sol. w/ xylene bubbles	7.81
Wetting Concent		0.0000	•	Average	7.23
OF1A OF1B OF1C	19 19 19	1 1 1	0.5 0.5 0.5	milky white	12.9
Wetting Concent		0.0245		Averàge	11.5
OF2A OF2B OF2C	19 19 19	1 1 1	1.0 1.0 1.0	milky white	6.83 10.4 8.64
Wetting Concent		0.0478	•	Average	8.62
OF3A OF3B OF3C	19 19 19	1. 1 - 1	2.0 2.0 2.0	grayish white	7.07 8.23
Wetting Concent		0.0913		Average	7.65
OF4A OF4B OF4C	19 19 19	1 1 1	4.0 4.0 4.0	amber gel	8.23 8.88
Wetting Concent		0.1673		Average	8.55

*Stepantex DA-52 **Xylene

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	Number	<u>(ml)</u>	<u>(ml)</u>	Agent (gram		Concentration (grams/cc)X	
•	OF5A OF5B OF5C	19.5 19.5 19.5	0.5 0.5 0.5	0 0 0	clear sol. w/ xylene bubbles	10.0 9.54	
	Wetting Concentr		0.0000	• • •	Average	9.77	
	OF6A OF6B OF6C	19.5 19.5 19.5	0.5 0.5 0.5	0.5 0.5 0.5	milky white	10.4 9.46 9.38	
	Wetting Concentr		0.0244		Average	9.74	
, -	OF7A OF7B OF7C	19.5 19.5 19.5	0.5 0.5 0.5	1.0 1.0 1.0	milky white	7.81 8.97	
•	Wetting Concentr		0.0477	•	Average	8.39	
·	OF8A OF8B OF8C	19.5 19.5 19.5	0.5 0.5 0.5	2.0 2.0 2.0	grayish white	8.23 9.05 6.91	
	Wetting Concentr		0.0911		Average	8.06	
	OF9A OF9B OF9C	19.5 19.5 19.5	0.5 0.5 0.5	4.0 4.0 4.0	amber gel	9.71 8.55	
	Wetting Concentr		0.1670		Average	9.13	

**Xylene

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Bottle Number	Water		rganic**	Wetting Agent* (grams)		Organic Vapor Concentration (grams/cc)X_10 ⁻⁶
OGOA OGOB OGOC	••• 19 19 19		1 · · · 1 1	0 0 0	clear sol. w/ xylene bubbles	6.74 6.25
Wetting Concent			0.0000		Average	6.49
OG1A OG1B OG1C	19 19 19		1 1 1	0.5 0.5 0.5	hazy-white &yellow residue on top	8.64 6.83
Wetting Concent			0.0245	•	Average	7.73
OG2A OG2B OG2C	19 19 19	•	1 1	1.0 1.0 1.0	hazy-white &(more)yellov residue on top	6.41 N 9.46
Wetting Concent		•	0.0478	• •	Average	7.93
OG3A OG3B OG3C	19 19 19		1 1 1	2.0 2.0 2.0	hazy yellow gel	9.05 10.0
Wetting			0.0913		Average	9.52
OG4A OG4B OG4C	19 19 19		1 1 1	4.0 4.0		6.00 6.83
Wetting Concent		·	0.1673	·	on top Average	6.41

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*Ninate 401 **Xylene

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Bottle Number	Water (ml)	Organic** <u>(ml)</u>	Wetting Agent* (grams)		Organic Vapor Concentration (grams/cc)X 10 ⁻⁶
0G5A 0G5B 0G5C	⁴⁴ 19.5 19.5 19.5	0.5 0.5 0.5	0 0 0	clear sol. w/ xylene bubbles	9.46 8.72
Wetting Concent:		0.0000	·.	Average	9.09
OG6A OG6B OG6C	19.5 19.5 19.5	0.5 0.5 0.5	0.5 0.5 0.5		7.48 8.31
Wetting Concent		0.0244		Average	7.89
OG7A OG7B OG7C	19.5 19.5 19.5	0.5 0.5 0.5	1.0 1.0 1.0	white hazy solyellow residue on bottom	6.74 7.07 7.73
Wetting Concent		0.0477		Average	7.18
OG8A OG8B OG8C	19.5 19.5 19.5	0.5 0.5 0.5	2.0 2.0 2.0	hazy sol. surrounding a yellow gel	7.81 8.64
· Wetting · Concent		0.0911		Average	8.22
OG9A OG9B OG9C	19.5 19.5 19.5	0.5 0.5 0.5	4.0 4.0 4.0	clear sol. surrounding a yellow gel w/ suspended white residue	8.88 8.64
Wetting Concent		0.1670		Average	8.76

*Ninate 401 **Xylene

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TABLE 127

Bottle Number	Water	Organic** (ml)	Wetting Agent* (grams)	Appearance	Organic Vapor Concentration (grams/cc)X 10
ОНОА ОНОВ ОНОС	³⁴ 19 19 19	1 1 1 1	0 0 0	clear w/ xylene bubbles	12.7 12.9
Wetting Concentr		0.0000		Average	12.8
OH1A OH1B OH1C	19 19 19	1 1 1	0.5 0.5 0.5	milky white	8.23 9.54
Wetting Concenti		0.0245	• •	Average	8.88
OH2A OH2B OH2C	19 19 19	1 1 1	1.0 1.0 1.0	milky white	11.8 11.0 11.7
Wetting Concent:		0.0478	•	Average	11.5
0H3A 0H3B 0H3C	19 19 19	1 1 1	2.0 2.0 2.0	hazy	9.46 7.48 11.4
Wetting Concent:		0.0913		Average	9.44
OH4A OH4B OH4C	19 19 19	1 1 1	4.0 4.0 4.0	hazy	10.2 13.2 11.7
Wetting Concent:		0.1673		Average	11.7
*Stepan				•	

**Xylene

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TABLE 127

•	Bottle Number	Water	Organic**	Wetting Agent*	Appearance	Organic Vap Concentrati	or on6
•		<u>(ml)</u>	(ml)	(grams)	and the state of t	(grams/cc)X	10-0
	OH5A OH5B OH5C	- 19.5 19.5 19.5	0.5 0.5 0.5	0 0 0	clear W/ xylene bubbles	11.1 9.87	••
•	Wetting Concent		0.0000		Average	10.5	
•	ОН6А ОН6В ОН6С	19.5 19.5 19.5	0.5 0.5 0.5	0.5 0.5 0.5	milky white	12.6 13.2	
•	Wetting Concent:		0.0244		Average	12.9	
	ОН7А ОН7В ОН7С	19.5 19.5 19.5	0.5 0.5 0.5	1.0 1.0 1.0	milky white	10.9	
	Wetting Concent		.0.0477	· · · · ·	Average	10.7	
	OH8A OH8B OH8C	19.5 19.5 19.5	0.5 0.5 0.5	2.0 2.0 2.0	hazy	$\frac{11.7}{11.7}$	
	Wetting Concent:		0.0911	•	Average	11.7	
	0H9A 0H9B 0H9C	19.5 19.5 19.5	0.5 0.5 0.5	4.0 4.0 4.0	hazy	11.8 10.7 10.8	
	Wetting Concent		0.1670		Average	11.1	
		· ·	·				

*Stepanate AM **Xylene

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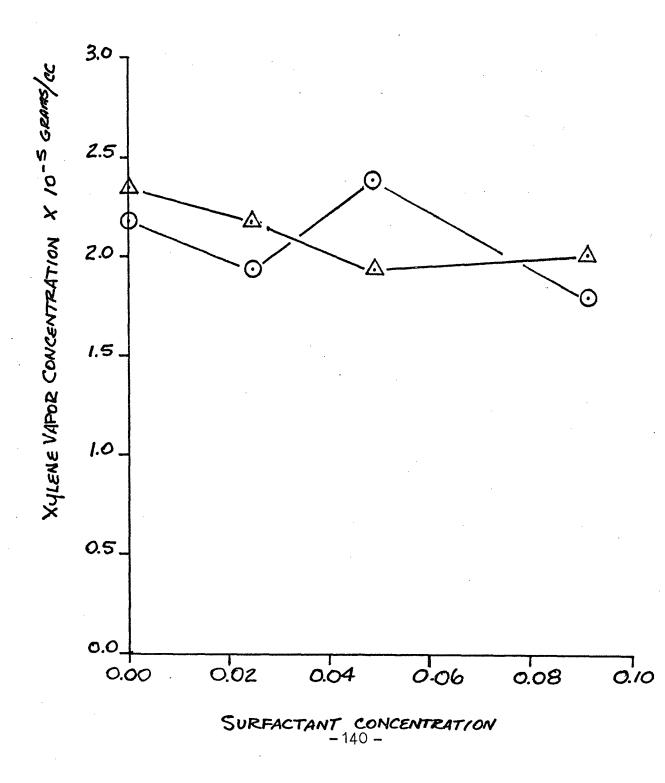
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FIGURES OF ORGANIC VAPOR CONCENTRATION VS. SURFACTANT CONCENTRATION

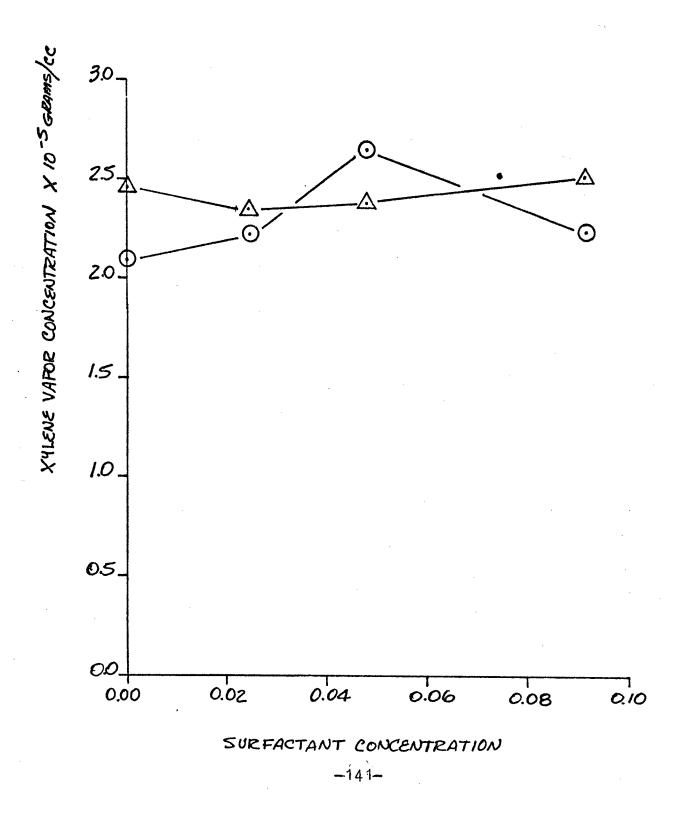
SURFACTANT - SANDOPAN DTC GEL PASTE

○ 19m\$ WATER & IMR XYLENE
△ 19.5ml WATER & O.Sml XYLENE

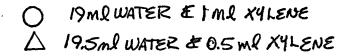


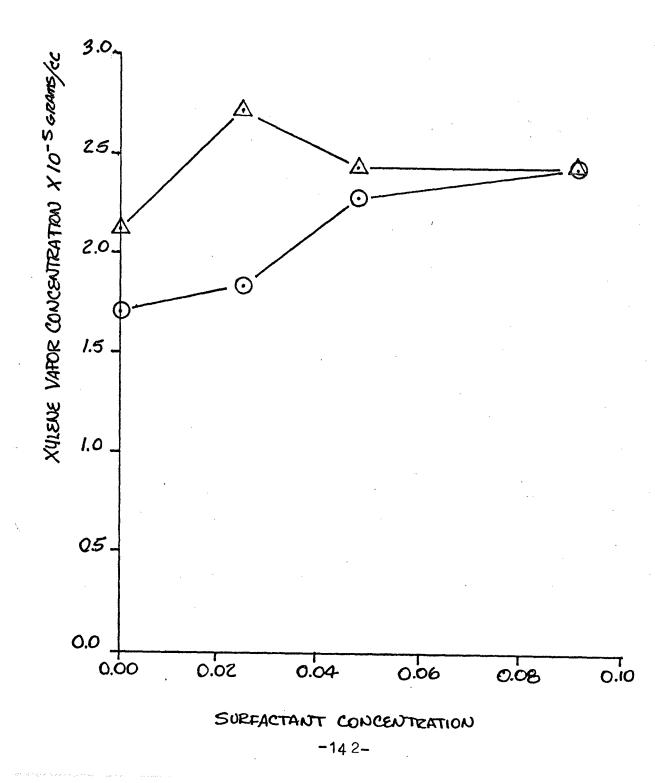
SUEFACTANT ULTRAWET 1565 (15.DS)

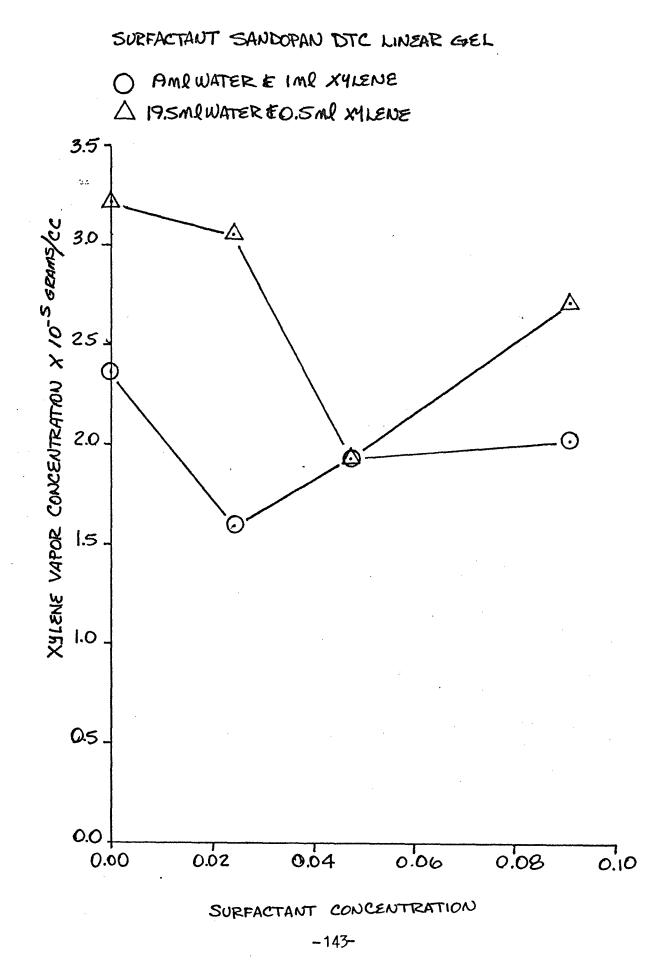
-) 19ML WATER & IML XYLENE
- △ 19.5ml WATER & O.5ml XYLENE



SURFACTANT 405X - LOT \$5212



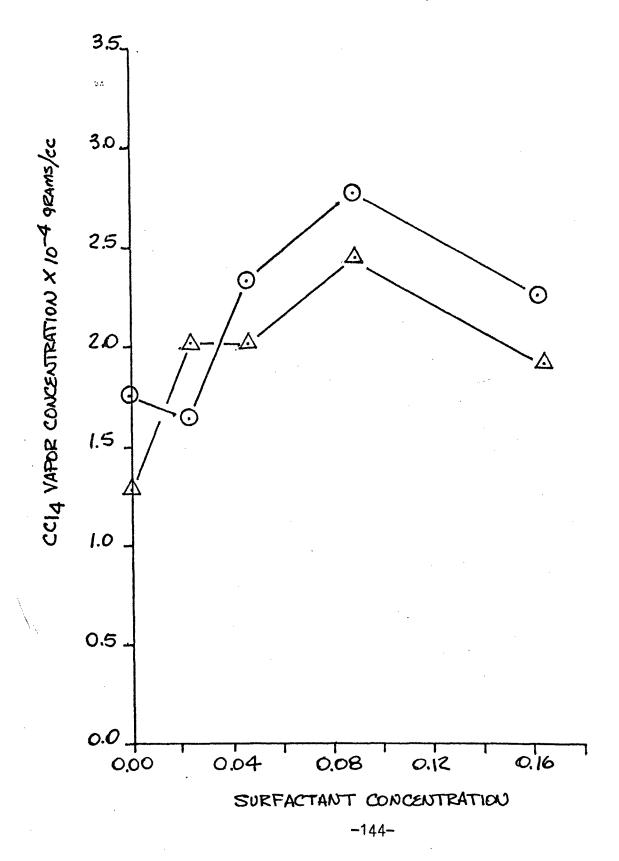


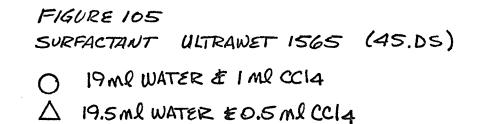


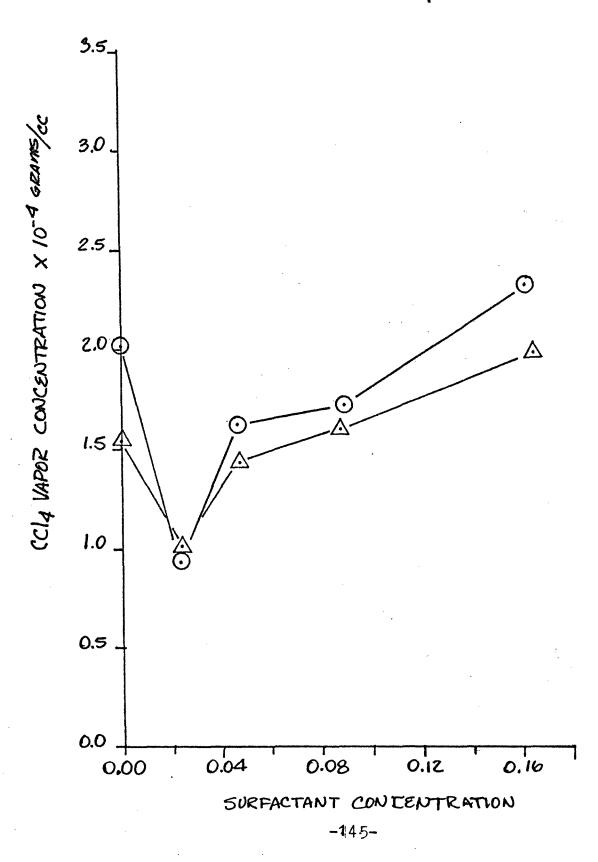
SURFACTANT SANDOPAN DTC GEL PASTE

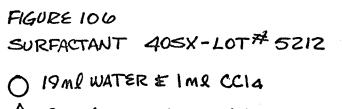
O I9ME WATER & IML CC14

△ P.SML WATER ± O.SML CC14

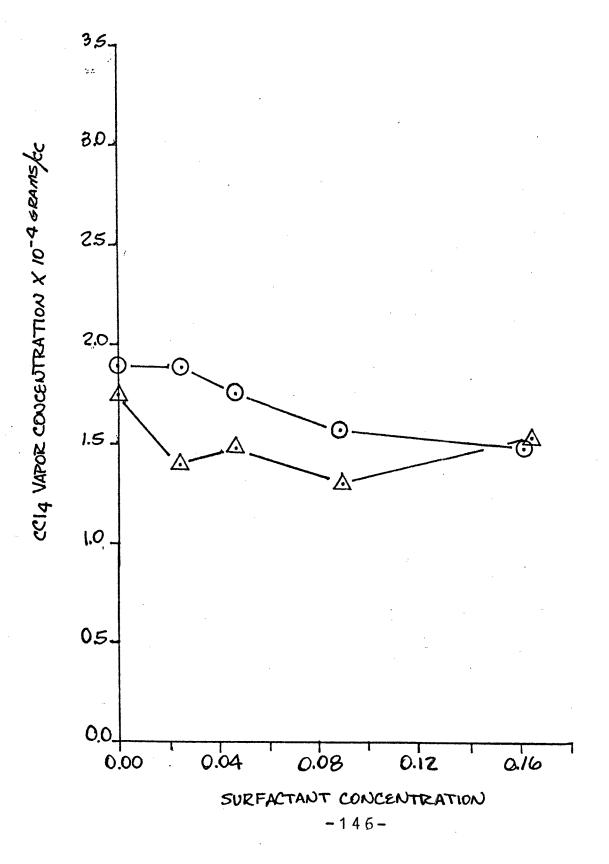












SURFACTANT SANDOPAN DTC LINEAR GEL

O 19 MQ WATER & IMPCC4

△ 19.5ml WATER & O.5ml CC14

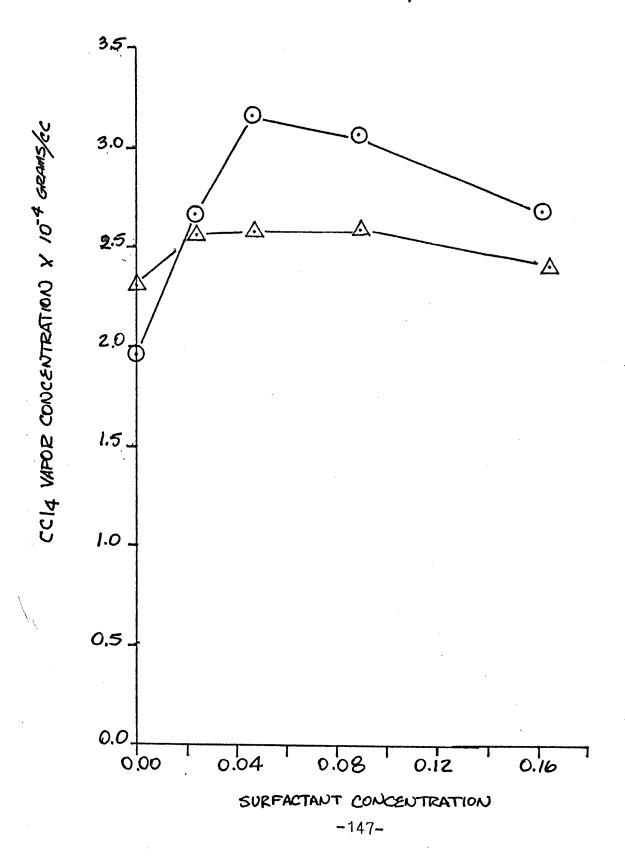


FIGURE 108 SURFACTANT SANDOPAN DTC GEL PASTE AMP WATER & IMP TOLUENE \bigcirc \triangle 19.5ML WATER & OSML TOLVENE 10.0_ ; TOLUENE VAPOR CONCENTRATION X10-5 984056 9.0 8.0. 7.0. . 60 5,0. А 4.0 \odot 3.0 0.04 0.02 0.06 0.00 0.08 0.10 SURFACTANT CONCENTRATION

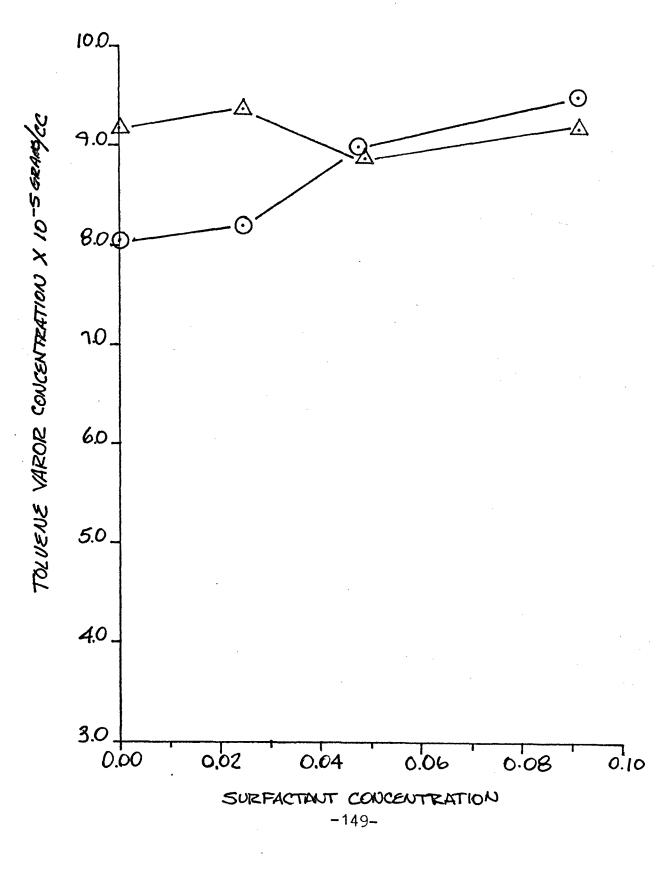
-148-

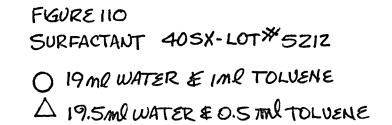
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SURFACTANT ULTRAWET 1565 (45.DS)

O 19 MQWATER & IMQ TOLUENE

△ 19.5ml WATER & O.5 Ml TOLVENE





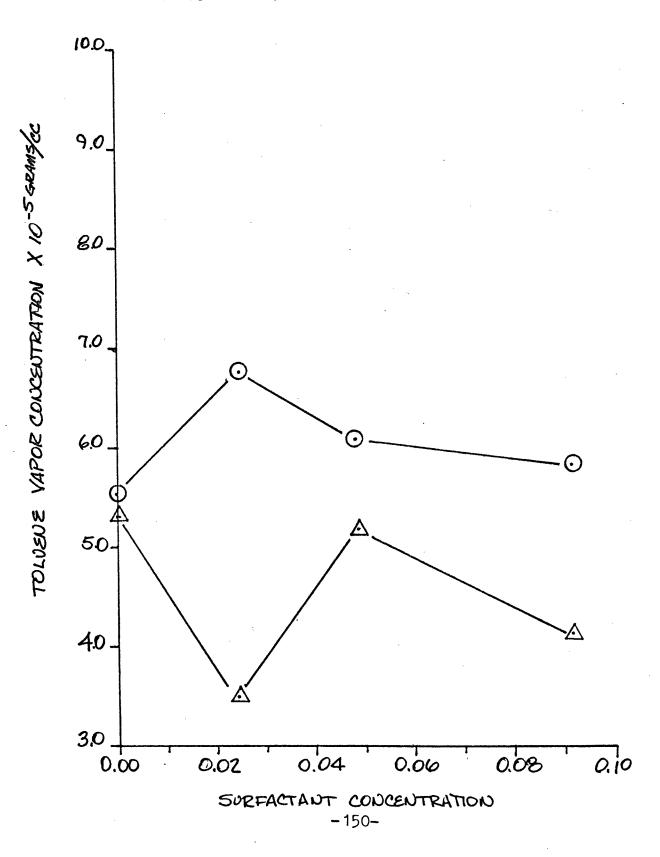


FIGURE III SURFACTANT SANDOPAN DTC LINEAR GEL O 19ML WATER & IML TOLUENE

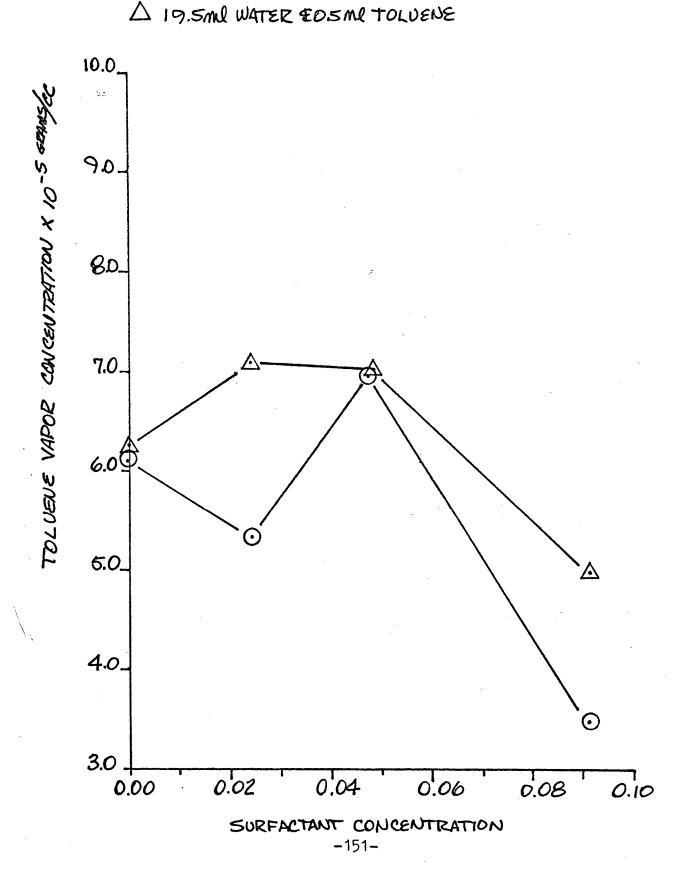


FIGURE 112 SURFACTANT SANDOPAN DTC GEL PASTE O 19MUL WATER & IMD ETHUL ACETATE \triangle 19.5MU WATER & 0.5MUL ETHUL ACETATE

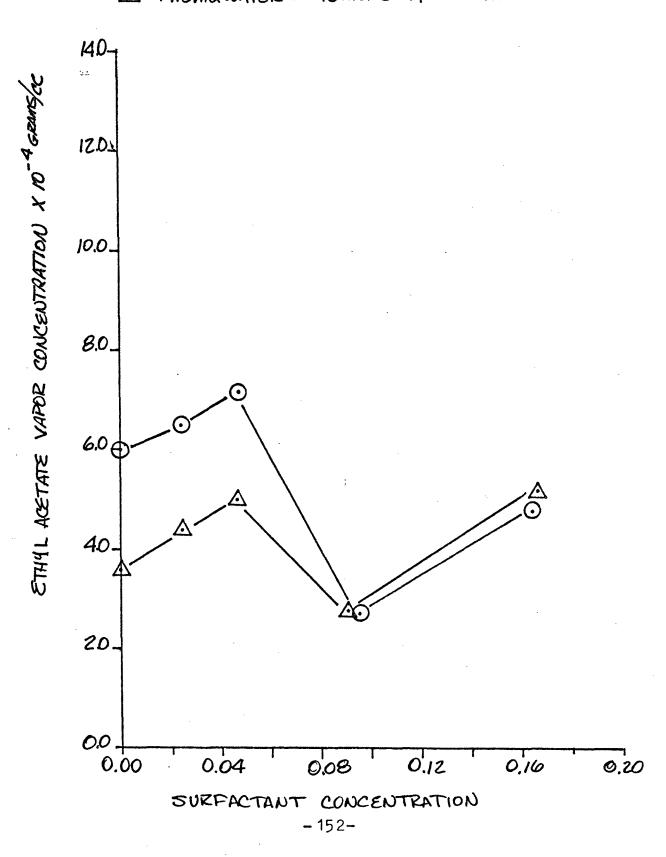


FIGURE 113 SUEFACTANT ULTEAWET 1565 (45.DS) O 19ml WATER & Imml ETHYL ACETATE \triangle 19.5ml WATER & 0.5ml ETHYL ACETATE

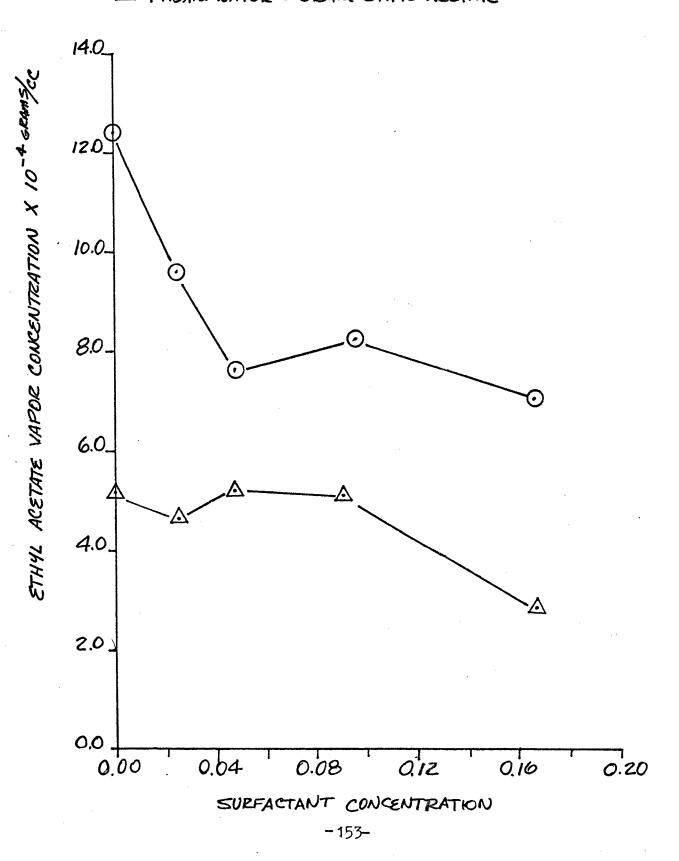


FIGURE 114 SURFACTANT 405X-LOT *5212

O 19 MU WATER & 1 MU ETHYL ACETATE

△ 19.5 M WATER & O.5 M ETHYL ACETATE

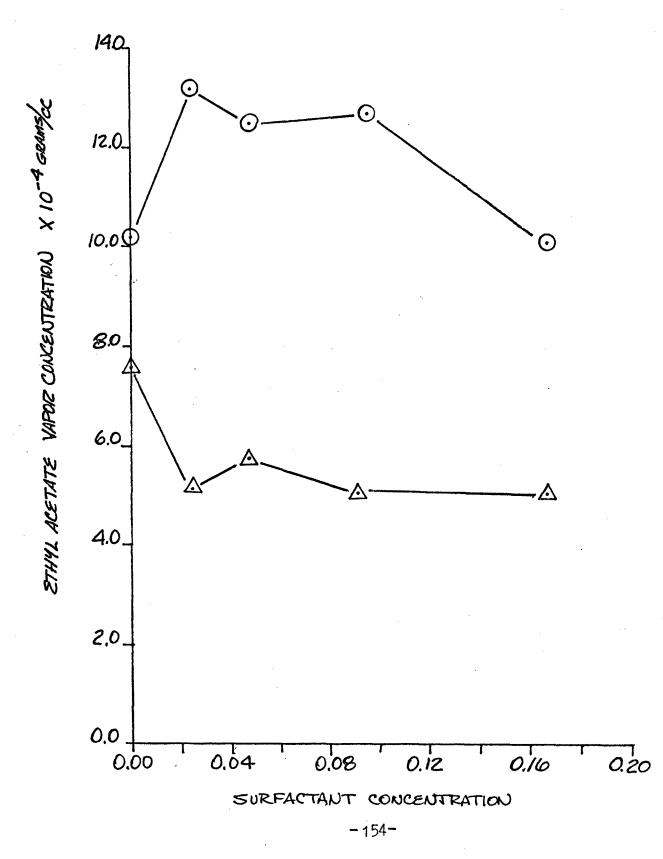
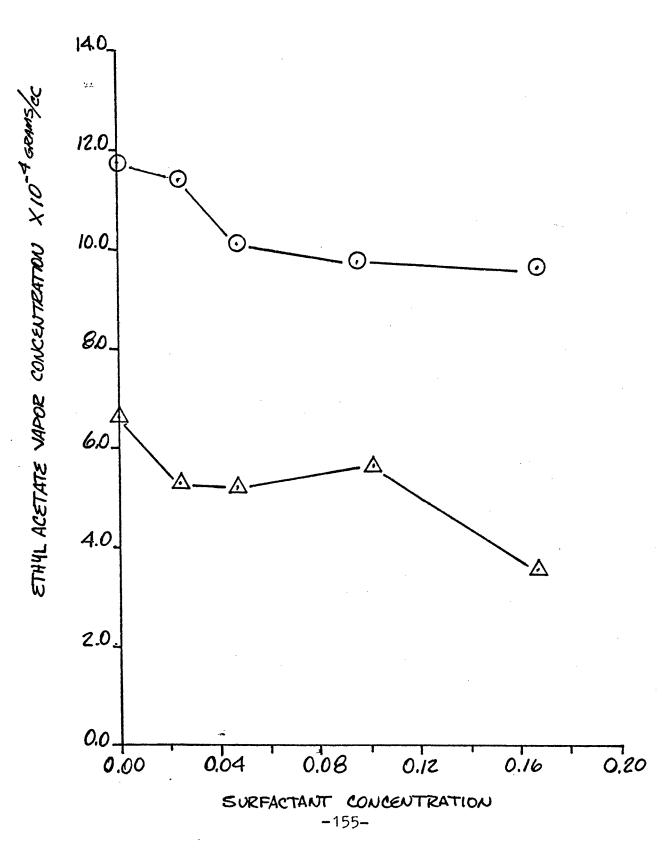
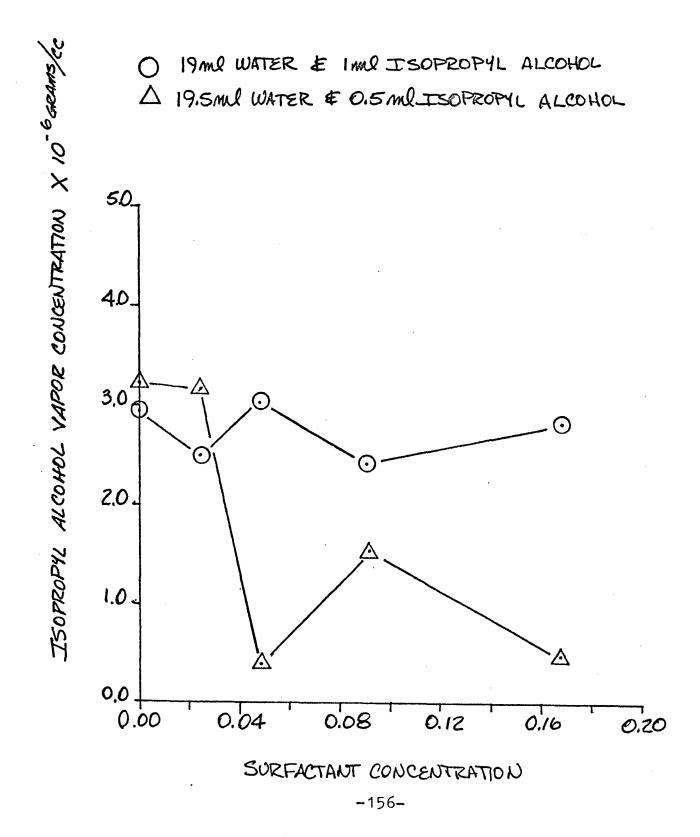


FIGURE 115 SURFACTANT SANDOPAN DTC LINEAR GEL O 19MI WATER & IMI ETHYL ACETATE

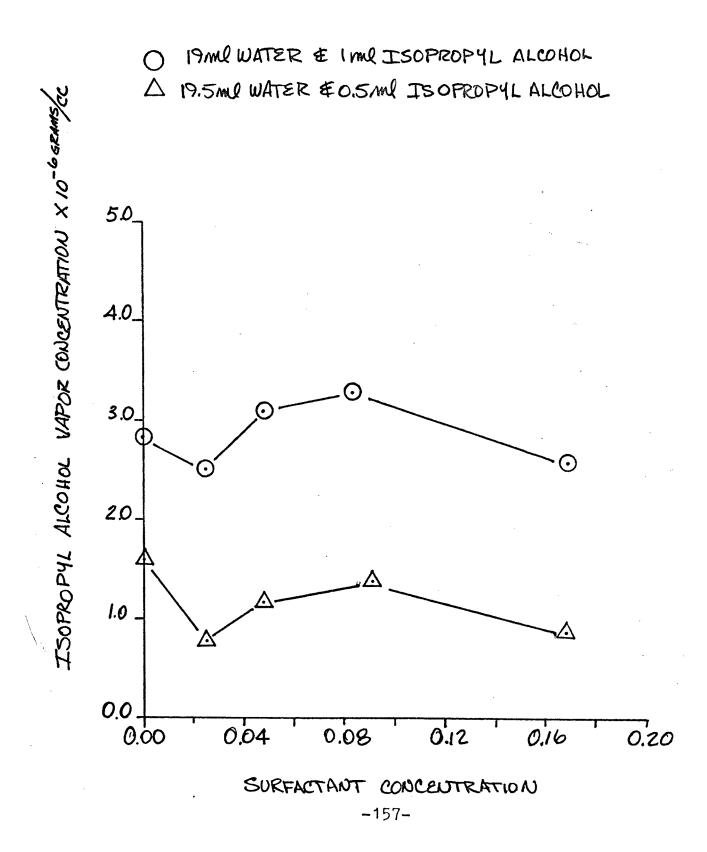
△ 19.5 M WATER & O.S.M ETHYL ACETATE



SURFACTANT SANDOPAN DTC GEL PASTE

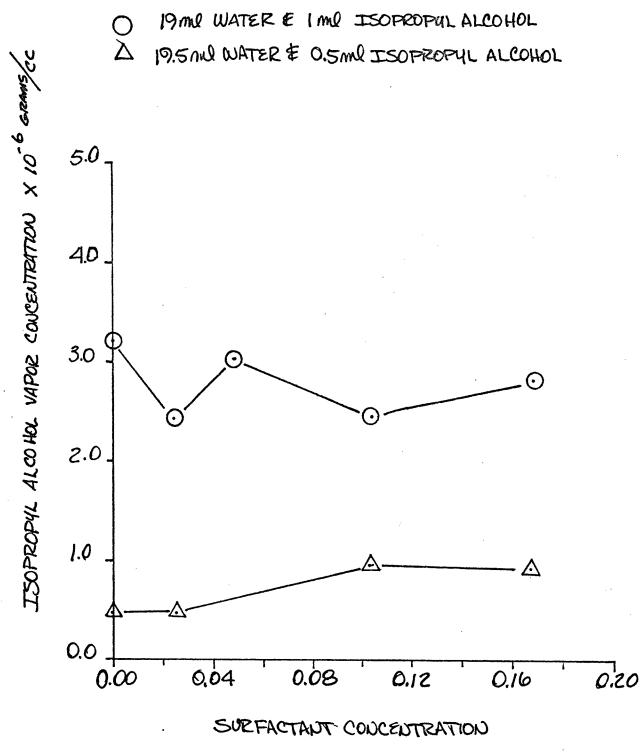


SURFACTANT ULTRAWET 1565 (45.DS)



FIGUREII8

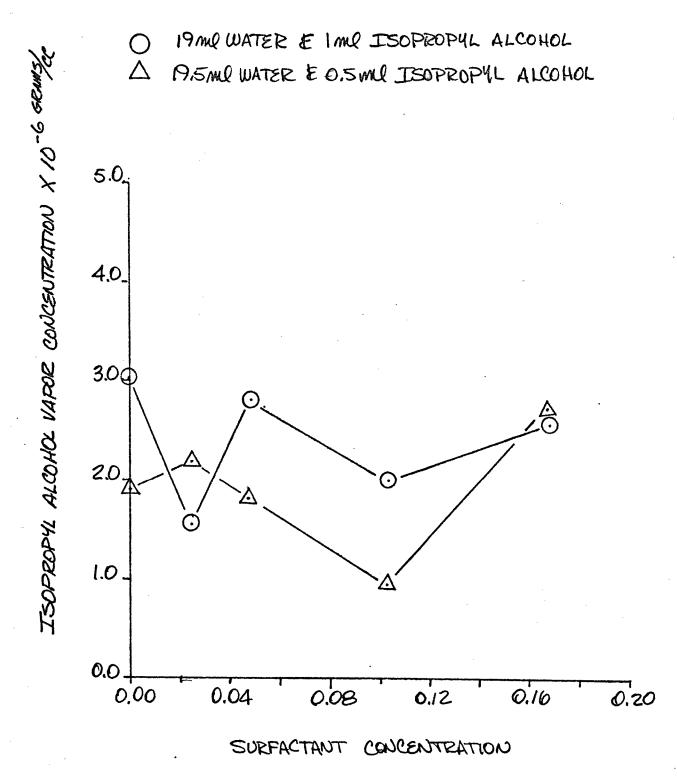
SURFACTANT 405X-LOT#5212

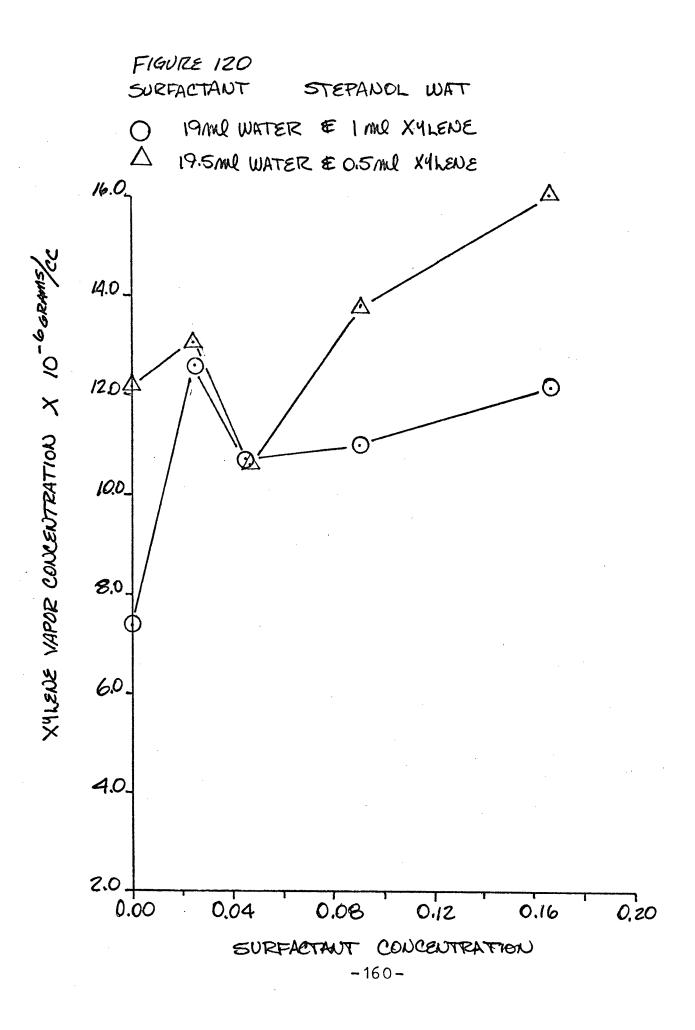


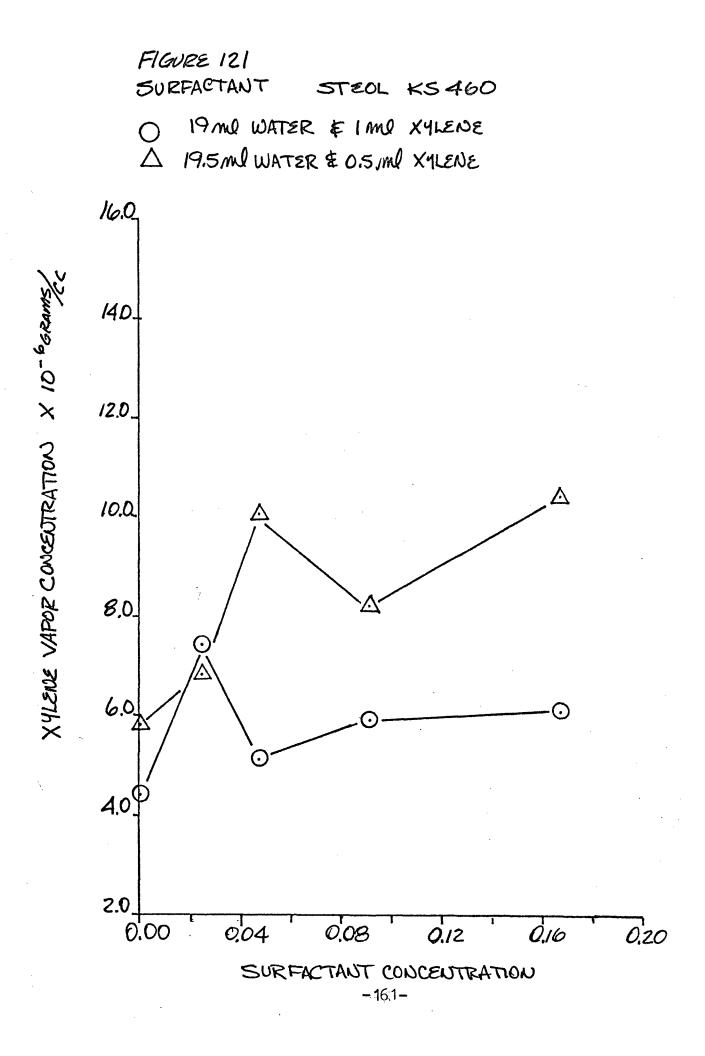
-158-

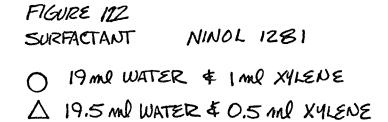
FIGURE IP

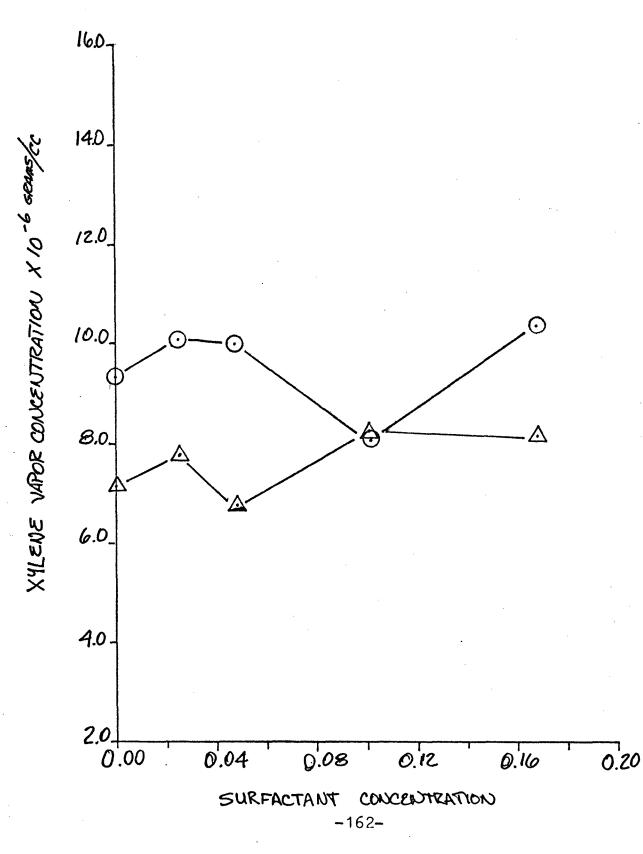
SURFACTANT SANDOPAN DTC LINEAR GEL

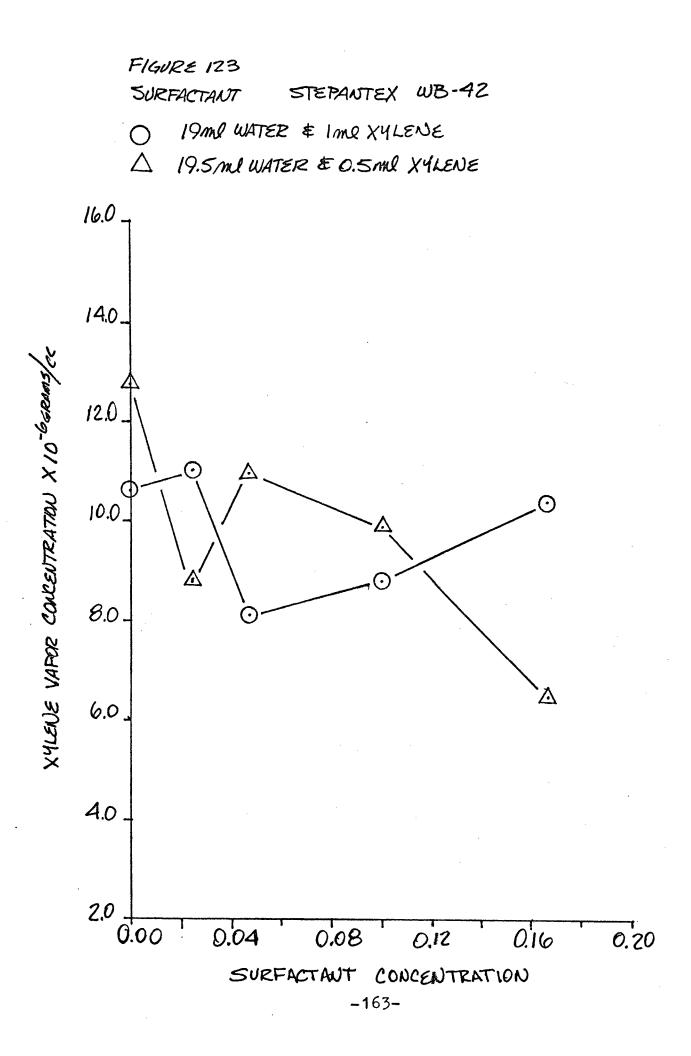






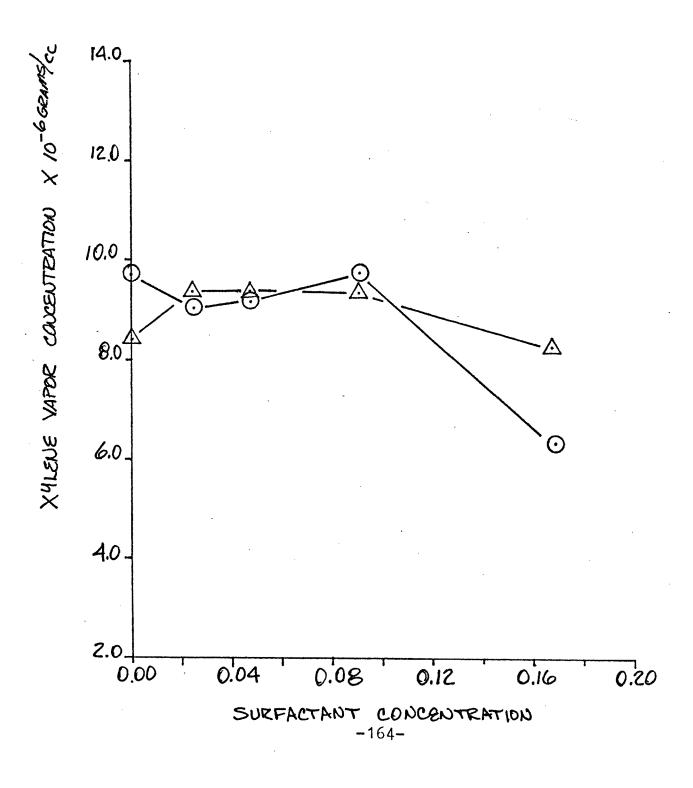




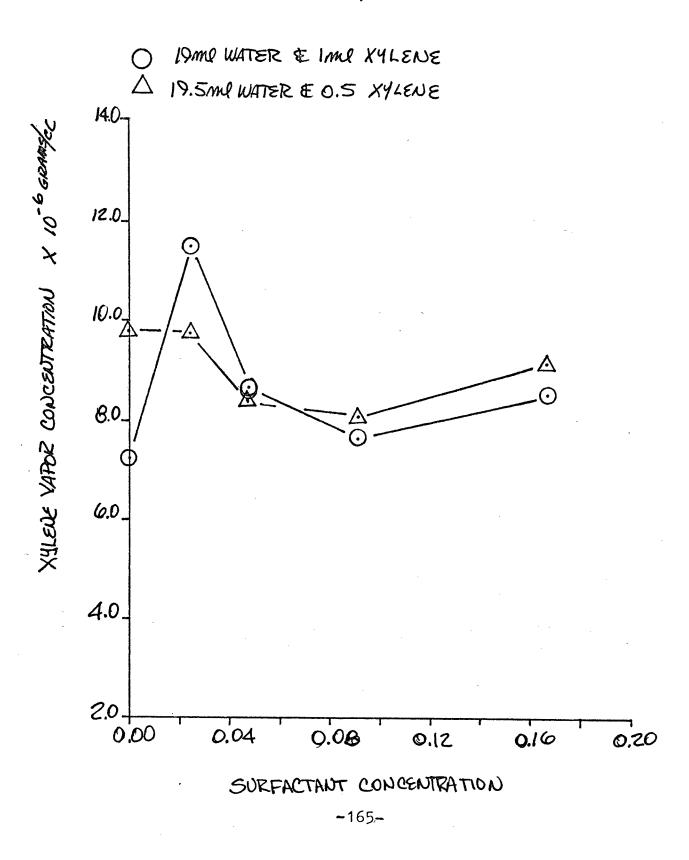


SURFACTANT TOXIMUL R

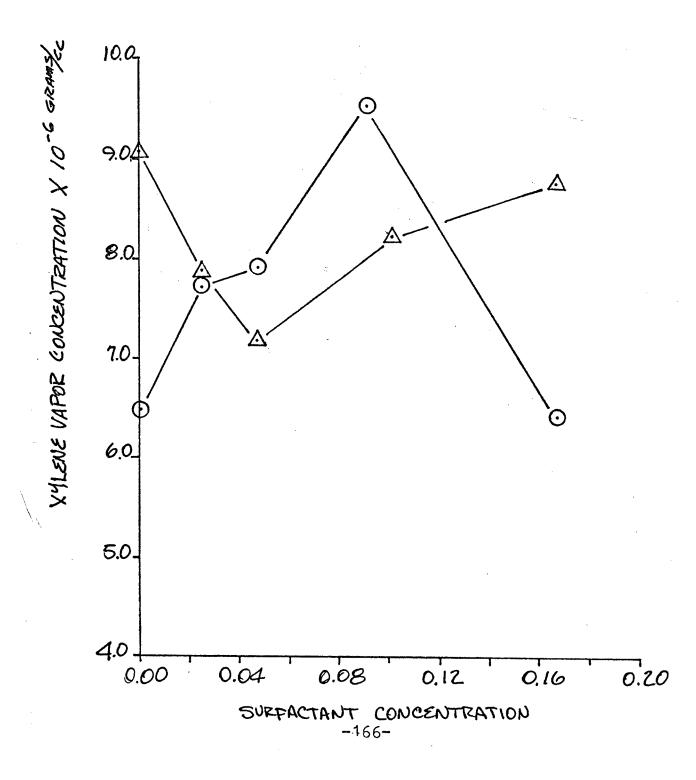
○ 19ml WATER € 1ml XYLENE
△ 195ml WATER € 0.5 ml XYLENE

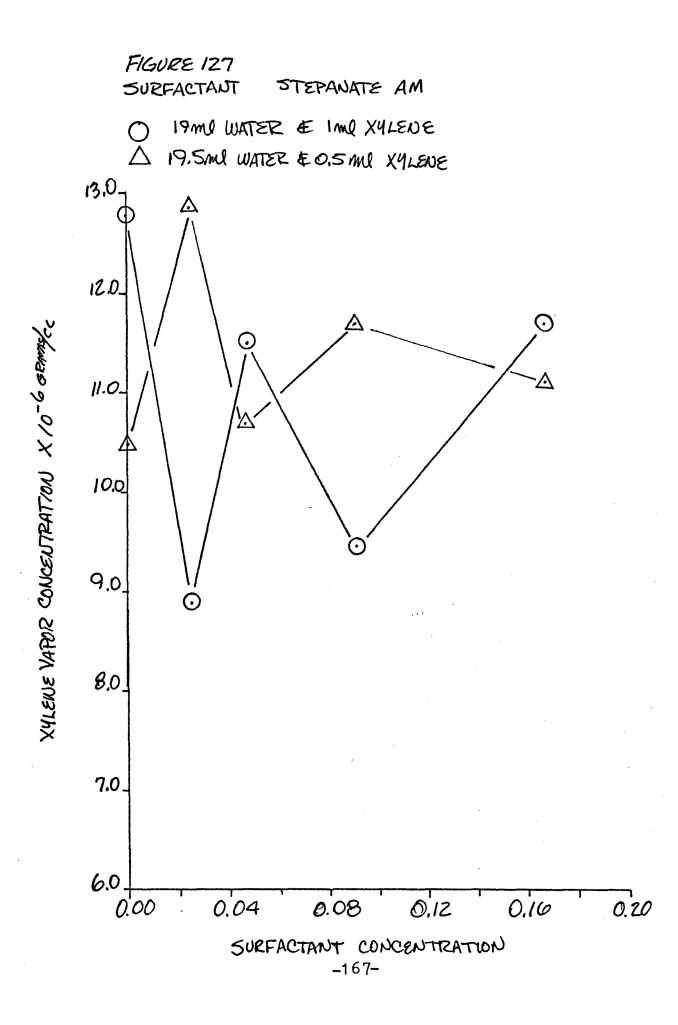


SURFACTANT STEPANTEX DA-52



SURFACTANT NINATE 401 O 19ml WATER & IML XYLENE A 19.5ml WATER & O.SML XYLENE





CHARTS OF ORGANIC RESULTANT SOLUBILITY DIFFERENTIAL

*CHART 100

. . .

<u>19.0 ml water1.0 ml organic</u> ** % surfactant	solubility change (per cent)
2.5	, 11 .
4.8	-10
9.2	17

19.5 ml water--0.5 ml organic**

	% surfactant	•
	2.5	3
	4.8	18
•	9.2	12

*For further data refer to Table or Figure with corresponding number

**Xylene

. _

-*CHART 101

<u>19.0 ml water1.0 ml organic**</u>	solubility change
% surfactant	(per cent)
2.5	-6
4.8	-26
9.2	-7

19.5 ml water--0.5 ml organic**

	% surfactant	
· . ·	2.5	6
	4.8	4
	9.2	-1.5

*For further data refer to Table or Figure with corresponding number •

•

**Xylene

•

.

19.0 ml water1.0 ml organic**	solubility change (per cent)
% surfactant	
2.5	-11.5
4.8	-34
9.2	-42

% surfactant	1	· · ·
% Surractant	e i i i i i i i i i i i i i i i i i i i	
2.5		-28
4.8		-15
9.2		-15

*For further data refer to Table or Figure with corresponding number

**Xylene

19.0 ml water1.0	ml_organic**	solubility change
»" % sur	factant	(per cent)
2.5		32
4.8		18
9.2		14

19.5 ml water--0.5 ml organic**

% surt	% surfactant	
2.5		5
4.8		39
9.2	•	.15

*For further data refer to Table or Figure with corresponding number

**Xylene

-171-

<u>19.0 ml water1.0 ml organic</u> ** % surfactant	solubility change (per cent)
2.4	6
4.6	-38
8.8	-57
16.2	-38

19.5 ml water--0.5 ml organic**

% surfactant	
2.4	-64
4.6	-67
8.8	-92
16.2	- 51

*For further data refer to Table or Figure with corresponding number •

•

**CCl4

.

*CHART 105

19.0 ml water1.0 ml organic**	solubility change (per cent)	
% surfactant		
2.4	66	
4.6	23	
8.8	19	
16.2	-11	
19 5 ml water0 5 ml organic**		

19.5 ml water--0.5 ml organic**

•

•••

% surfactant	•		•
2.4			30
4.6		,	7
8.8	• • •		- 3
16.2			-22
•		• • • • • • • • • • • • • • • • • • •	

· · · · · · · · · ·

*For further data refer to Table or Figure with corresponding number

**CC14

.

19.0 ml water1.0 ml organ	solubility change (per cent)
% surfactant	
2.4	- 1
4.6	6
8.8	16
16.2	21
•	
<u>19.5 ml water0.5 ml organ</u>	nic**
% surfactant	
2.4	19
4.6	15
4.0	
8.8	25
	•

**CC14

•

-*CHART 107

19.0 ml water1.0 ml organic**	solubility change	
% surfactant	(per cent)	
2.4	- 35	
4.6	-60	
8.8	- 55	
16.2	-37	

19.5 ml_water--0.5 ml_organic**

% surfactant	
2.4	-11
4.6	-13
8.8	-16
16.2	- 4

•

*For further data refer to Table or Figure with corresponding number

**cc14

.

· · · · · ·

*CHART 108

.

19.0 ml water1.0 ml organic**	solubility change (per cent)
% surfactant	
2.5	- 7
4.8	- 4
9.2	39

19.5 ml water--0.5 ml organic**

.

% surfactant	
2.5	1
4.8	12
9.2	18

.

*For further data refer to Table or Figure with corresponding number

**Toluene

19.0 ml water1.0 ml organic** % surfactant	solubility change (per cent)
·	
2.5	- 2
4.8	-12
9.2	-18

19.5 ml water--0.5 ml organic**

% surfactant	
2.5	- 2
4.8	4
9.2	0
	· · · ·

*For further data refer to Table or Figure with corresponding number *Toluene

**Toluene

.

<u>19.0 ml water1.0 ml organic</u> ** % surfactant	solubility change (per cent)
2.5	-23
4.8	-10
9.2	- 6

19.5 ml water--0.5 ml organic**

% surfactant	
2.5	34
4.8	2
9.2	22
	•

*For further data refer to Table or Figure with corresponding number

**Toluene

*CHART 111

.

<u>19.0 ml water1.0 ml organic</u> ** % surfactant	solubility change (per cent)
2.5	13
4.8	-14
9.2	43

19.5 ml water--0.5 ml organic**

% surfactant	
2.5	-13
4.8	-13
9.2	21

*For further data refer to Table or Figure with corresponding number

**Toluene

-*CHART 112.

<u>19.0 ml water1.0 ml organic</u> ** % surfactant	solubility change (per cent)
2.5	- 9
4.8	-20
9.6	55
16.7	20

19.5 ml water--0.5 ml organic**

% surfactant	· ·	
2.5	•	-22
4.8		-41
9.6	•	23
16.7		- 55

*For further data refer to Table or Figure with corresponding number

**Ethyl Acetate

.

19.0 ml water1.0 ml organic**	solubility change (per cent)
% surfactant	
2.5	23
4.8	39
9.6	34
16.7	43

19.5 ml water0.5 ml organic**	
% surfactant	
2.5	11
4.8	- 1
9.6	· · · 1
16.7	45

v** Ethyl Acetate

19.0 ml water1.0 ml organic**	solubility change
% surfactant	(per cent)
2.5	-29
4.8	-23
9.6	-24
16.7	1 · · · · · · · · · · · · · · · · · · ·

19.5 ml water--0.5 ml organic**

% surfactant	
2.5	32
4.8	24
9.6	
16.7	40

*For further data refer to Table or Figure with corresponding number

**Ethyl Acetate · ·

-*CHART 115

solubility change (per cent)
· ·
3
14
17
18
· · · · · · · · · · · · · · · · · · ·
20
21
15
46

*For further data refer to Table or Figure with corresponding number

**Ethyl Acetate

,

.

.

<u>19.0 ml water1.0 ml organic</u> **	solubility change (per cent)
% surfactant	
2.5	15
4.8	- 2
9.2	18
16.8	5
<u>19.5 ml water0.5 ml organic**</u>	· · ·
% surfactant	
2.5	2
4.8	88
9.2	53
16.8	87
	· · · · · ·

*For further data refer to Table or Figure with corresponding number

**Isopropyl Alcohol.

. . •

· ·

<u>19.0 ml water1.0 ml organic</u> ** % surfactant	solubility change (per cent)
2.5	12
4.8	- 9
9.2	- 15
16.8	8
19.5 ml water0.5 ml organic**	
% surfactant	

.50
27
13
46

*For further data refer to Table or Figure with corresponding number

**Isopropyl Alcohol

. .

*CHART 118

<u>19.0 ml water1.0 ml organic**</u>	solubility change (per cent)
% surfactant	
2.5	24
4.8	6
9.2	. 25
16.8	12

19.5	ml	water	-0.5	ml	organic**
------	----	-------	------	----	-----------

% surfactant	
2.5	0
4.8	_
9.2	-95
16.8	-90
	<u>.</u>

**Isopropyl Alcohol

<u>19.0 ml water1.0 ml organic</u> ** % surfactant	solubility change (per cent)
2.5	48
4,8	7
9.2	33
16.8	15

19.5 ml water--0.5 ml organic**

% surfactant	· · · ·
2.5	-15
4.8	5
9.2	50
16.8	-42

*For further data refer to Table or Figure with corresponding number

**Isopropyl Alcohol

-**CHART 120

19.0 ml water1.0 ml organic**	solubility change (per cent)	
% surfactant	(per cent)	
2.5	-70	
4.8	-45	
9.1	-49	
16.7	-65	

19.5 ml water--0.5 ml organic**

.

% surfactant	
2.5	- 7
4.8	16
9.1	-13
16.7	-31

•

*For further data refer to Table or Figure with corresponding number

**Xylene

<u>19.0 ml water1.0 ml organic</u> ** % surfactant	solubility change (per cent)
2.5	-69
4.8	-22
9.1	-35
16.7	-40

<u>19.5 ml water--0.5 ml organic**</u>

% surfac-	tant	
2.5		-18
4.8		-87
9.1		-42
16.7		-79

*For further data refer to Table or Figure with corresponding number

**Xylene

<u>19.0 ml water1.0 m</u>	l_organic**	solubility cha	ange
% surf	actant	(per cent	
2.5		- 8	•
4.8		- 7	
9.2		14	
16.7		-11	
			•
<u>19.5 ml water0.5 m</u>	l_organic**		• •
% surf	actant		
2.5		- 9	•
4.8		5	
9.1		-16	
16.7		-15	
	· · · ·	· ·	•

**Xylene

19.0 ml water1.0 ml organic**	solubility change (per cent)
% surfactant	(Per Cent)
2.5	- 3
4.8	24
9.1	17
16.7	2
19.5 ml water0.5 ml organic**	
% surfactant	
2.5	31

14

.23

49[°]

*For	further	data	refer	to	Table	or	Figure	

with corresponding number

4.8

9.1

16.7

. •

**Xylene

.

*CHART 124

r 1 10 a

19.0 ml water1.0 ml organic**	solubility change
% surfactant	(per cent)
2.5	7
4.8	6
9.1	0
16.7	36
19.5 ml water0.5 ml organic**	
% surfactant	
2.5	-11
4.8	-11
9.1	-10
16.7	2

*For further data refer to Table or Figure with corresponding number

**Xylene

. . .

 19.0 ml water--1.0 ml organic**
 solubility change (per cent)

 % surfactant
 -59

 4.8
 -19

 9.1
 -6

 16.7
 -18

19.5 ml_water--0.5 ml_organic**

% surfactant

2.5	0	
4.8	14	-
9.1	18	
16.7	7	

*For further data refer to Table or Figure with corresponding number

**Xylene

...

**CHART 126

<u>19.0 ml water1.0 ml organic**</u>	solubility change (per cent)		
% surfactant			
2.5	-19		
4.8	-22		
9.1	-47		
16.7	1		

19.5 ml water--0.5 ml organic**

% surfactant	, ,	
2.5	13	
 4.8	21	
9.1	 10	
16.7	4	
· · ·		

·

*For further data refer to Table or Figure with corresponding number .

**Xylene

•

19.0 ml water1.0 ml organic** % surfactant	solubility change (per cent)	
2.5	31	
4.8	10	
9.1	26	
16.7	9	

<u>19.5 ml w</u>	<u>ater0.5 n</u>	<u>nl organic</u> **	f	
	% surf	factant		· ·
	2.5			-23
•	4.8			- 2
	9.1			-11
	16.7	•	· · · ·	6

•

**Xylene

.