



FACULTY OF ENGINEERING AND ARCHITECTURE

An experimental and theoretical study of cyclopentadiene-ethene copyrolysis: Growth of polycyclic aromatic hydrocarbons

M.R. Djokic<sup>a</sup>, A.G. Vandeputte<sup>b</sup>, S.S. Merchant<sup>b</sup>, W.H. Green<sup>b</sup>, K.M. Van Geem<sup>a</sup>, G.B. Marin<sup>a</sup>

<sup>a</sup> Laboratory for Chemical Technology, Technologiepark 914, 9052 Ghent, Belgium



<sup>b</sup> Department of Chemical Engineering, MIT, Cambridge, MA, USA

http://www.lct.UGent.be E-mail: Marko.Djokic@UGent.be



Introduction

• Polycyclic aromatic hydrocarbons (PAHs) are a group of more than 100 chemicals

## **Role of CPD and CPDyl**

The **CPDyl** radical is a resonance-stabilized, ambident, i.e. containing multiple reactive

that can be produced from various anthropogenic sources, such as the incomplete combustion of heating fuels, oil refining processes and the combustion of diesel fuels •Many **PAHs** are known to be **carcinogenic** or **mutagenic** and important precursors to soot, which has been linked to human morbidity and global warming

potential soot precursors' reactions those involving the • Among many cyclopentadiene (CPD) and its corresponding cyclopentadienyl (CPDyl) radical are considered to be one of the most important contributors to **PAHs** and **soot formation** 

- centers, radical that may undergo self-recombination reactions
- Due to its importance significant amount of experimental and theoretical data has been published on the gas phase chemistry involving **CPDyl** and **CPD** in the growth of **PAHs**
- This work deals both **experimentally** and **theoretically** with the growth of **PAHs** starting from **CPD** and **CPDyl**









Use of reference components in the product analysis section (RGA, GC×GC)





Schematic diagram of the experimental set-up indicating process gas temperatures (Ti) and pressure measurements (CIP & COP) (1-electronic balance; 2-liquid feed reservoir (DCPD); 3-gaseous diluent/internal standard (nitrogen/ethene); 4-pressure reducing valve; 5-coriolis flow meter controlled pump; 6-coriolis mass flow controller; 7-valve; 8-evaporator/heater; 9-mixer; 10heater; 11-heated sampling oven; 12-GC×GC-FID/TOF-MS for C5+; 13-outlet pressure restriction valve; 14-cyclone separator; 15-condenser; 16-dehydrator; 17-Refinery Gas Analyzer (RGA) for C4-; 18-data acquisition system)

•Djokic et al. Combust. Flame. 2014

<u>2-norbornene</u>

Good match!



## Experimental conditions:

Co-pyrolysis of **CPD-ethene** mixture

✓ A tubular continuous flow reactor (Incoloy 800HT; 1.5 m L.; 6 mm I.D.)

 $\checkmark$  T<sub>reactor</sub>= 873 - 1163 K, nearly **isothermal**, COP=1.7 bara,

- Nitrogen was used as a diluent and primary **Internal standard**
- ✓ **Dilution** of 1 mol CPD/ 1 mol C<sub>2</sub>H<sub>4</sub>/ 10 mol N<sub>2</sub>, F<sub>0 CPD</sub>=13.6 mg/s
- ✓ **Argon** was used as additional (as a double-check) internal standard
- On-line sampling of the effluent using **heated transfer lines** (573 K)
- ✓ Dedicated analysis section: GC×GC-FID/TOF-MS + RGA(FID, TCD)

Thermo Scientific Tempus **TOF-MS** 

•Van Geem, Pyl, et al. J. Chromatogr. A. 2010

473 K

**▲**source



## **Experimental and Kinetic Modeling Results**

65.0 67.0 77.0 79.0 48.2 50.0 1 1 52.1 61.0 62.0 668.1 69.8 74.0 77.5

Conditions							
Temperature (K)	873	923	973	1023	1073	1123	116
CPD flow rate (g/h)	49	49	49	49	49	49	49
Ethene flow rate (g/h)	21	21	21	21	21	21	21
$N_2$ flow rate (g/h)	206	206	206	206	206	206	20
CPD Conversion (%)	1.2	1.8	5.0	15.6	37.8	71.6	92.
Yield (wt%)							

H <sub>2</sub>	0.00	0.01	0.02	0.09	0.20	0.69	1.19			
CH <sub>4</sub>	0.00	0.02	0.11	0.36	1.13	2.97	4.09			
Alkenes										
Ethene	29.92	29.81	29.50	29.08	29.14	26.61	24.50			
Cyclopentadiene	69.16	68.76	66.47	59.09	43.57	19.88	5.35			
Aromatics										
Benzene	0.01	0.03	0.21	1.16	2.77	8.56	11.68			
Toluene	0.02	0.00	0.03	0.18	0.43	1.98	3.74			
Styrene	0.00	0.00	0.01	0.00	0.17	0.92	2.43			
Indene	0.03	0.08	0.56	2.03	4.82	7.63	5.95			
Naphthalene	0.05	0.09	0.40	2.33	7.19	16.74	20.44			
Phenantherene	0.00	0.00	0.00	0.02	0.44	1.29	2.35			
Anthracene	0.00	0.00	0.00	0.03	0.37	0.81	1.39			
Total PAHs	0.48	0.77	2.47	7.82	20.36	35.18	43.55			
$(y_{M})$ $(y_{$	35 30 25 20 15 10 10 10 14 1.2 10 10 1.4 1.2 10 0.0 1.4 1.2 1.0 8.0 0.0 1.4 1.2 0.0 0.0 1.4 1.2 0.0 0.0 1.4 1.2 0.0 0.0 1.4 1.2 0.0 0.0 1.5 1.0 0.0 0.0 1.5 0.0 0.0 1.5 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0	C <sub>2</sub> H <sub>4</sub> 900 100 Tempe 1,3-C <sub>4</sub> 900 100 Tempe	Do 1100 rature (K) H <sub>6</sub>	1200 1000 120 12	$H_2$ $H_2$	1000 mperature	(K)			
Current model predictions (full lines) of the main reaction products										

## **Kinetic Modeling**

- A single-event microkinetic model was generated using an automated reaction network generator, **RMG**
- Parameters requiring refinement are identified through sensitivity analysis
- **No fitting** of the parameters to the experimental data
- Individual reactions are subjected to an increased level of theoretical analysis
- Thermodynamics and kinetic data of sensitive species and reactions were calculated using quantum chemistry calculations at the **CBS-QB3** level using Gaussian 03 Conclusions Dedicated **GC×GC** setup combining **FID** and **TOF-MS** Implemented in an **on-line** analysis section of a bench scale set-up for (steam) **co-pyrolysis of CPD/C<sub>2</sub>H<sub>4</sub>** Detection of **PAHs** up to carbon number  $C_{20}$ Excellent agreement between **experiments** and **theory** Acknowledgment The work at the LCT was supported by the 'Long Term' Structural Methusalem Funding by the Flemish Government'.

- A very complex product spectrum strongly depending on the temperature
- At 923 K only limited number of pyrolysis products can be detected such as C<sub>7</sub>H<sub>10</sub> species, norbornene, indene, naphthalene, benzene and cyclopentene

**TOF-MS** 



- At 1073 K the reactor effluent is significantly more complex, containing on the order of up to **hundred different compounds** at the highest temperature
- At the most severe conditions, 92% of CPD is converted yielding almost 44 wt% of PAHs with a carbon number up to  $C_{20}$

The work at the MIT was supported by the Combustion Energy Frontier Research Center, funded by the U.S. Department of Energy, Office of Basic Energy Sciences under award number DE-SC0001198.

9<sup>th</sup> International Conference on Chemical Kinetics, Ghent, 28 June - 2 July, 2015