

Ab initio based micro-kinetic modeling of benzene hydrogenation on Pd(111), as a function of hydrogen coverage

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Catalytic hydrogenation of benzene

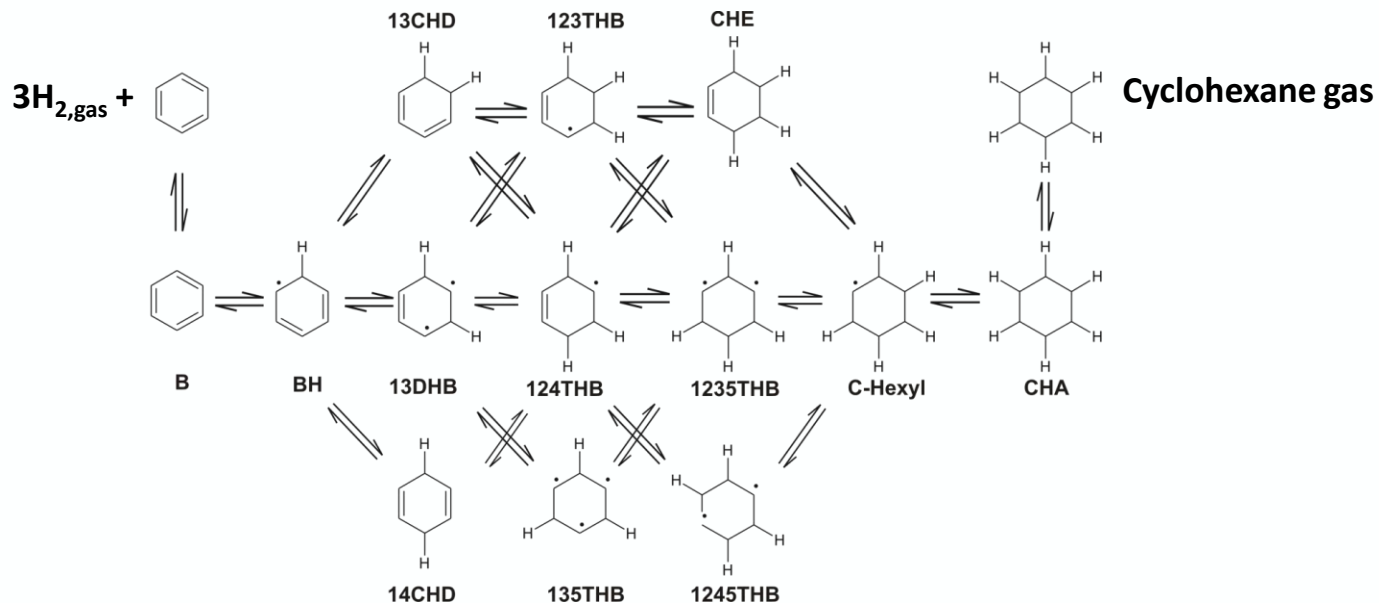
Industrial applications:

- Hydrotreating of fuels
- Petrochemical industry (nylon)

Environmental applications:

Production of clean fuels
(benzene is carcinogen type A)

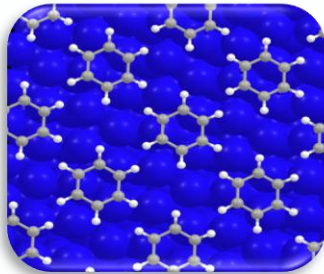
- ❑ Complex catalytic reaction network, with multiple possible adsorption sites
- ❑ For one adsorption site → full network with 13 intermediates
- ❑ Palladium is a widely used catalyst for hydrogenation reactions
- ❑ Pd(111) is the most abundant and stable surface



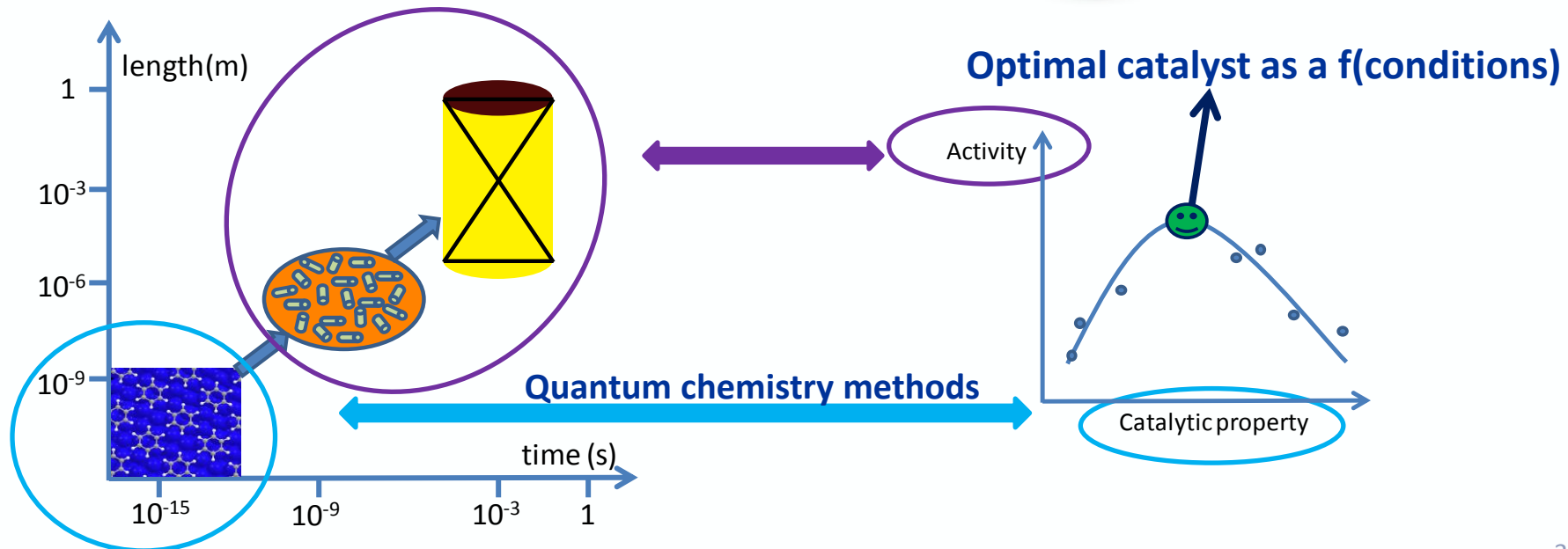
Integrating theoretical models into industry

Important goal in industry:
developing new catalysts with novel catalytic properties

Ab initio based kinetics



Industrial models



Outline

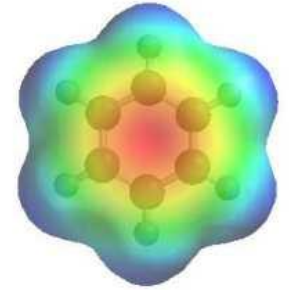
- Introduction
- Methodology
- Results
- Conclusions

Density Functional Theory (DFT)

Idea of DFT: minimize energy with respect to the electron density

The energy is a functional of ρ :

$$E[\rho] \rightarrow \rho(r) \rightarrow r(x,y,z)$$



$$E[\rho] = \underbrace{-\frac{1}{2} \sum_{i=1}^n \int \phi_i^*(r_i) \nabla^2 \phi_i(r_i) dr_i}_{\text{Kinetic energy}} - \underbrace{\sum_{x=1}^N \frac{Z_x}{r_{xi}} \rho(r_i) dr_i}_{\text{Nuclear-electron interactions}} + \underbrace{\frac{1}{2} \iint \frac{\rho(r_1)\rho(r_2)}{r_{12}} dr_1 dr_2}_{\text{Coulombic repulsions}} + E^{xc}[\rho]$$

Exchange and correlation functional

Biggest challenge → source of inaccuracy

Different approximations:

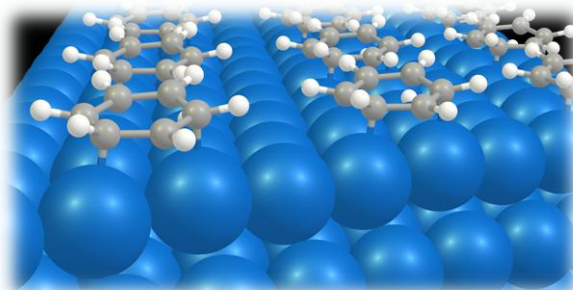
This work uses the Generalized gradient approximation (PW91)

Computational approach: catalyst model & DFT

Periodic DFT calculations

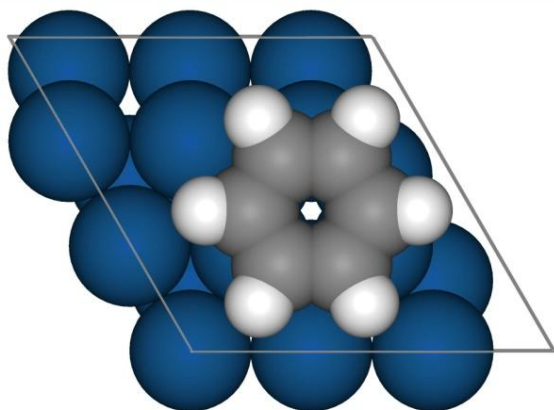


fcc Pd(111)



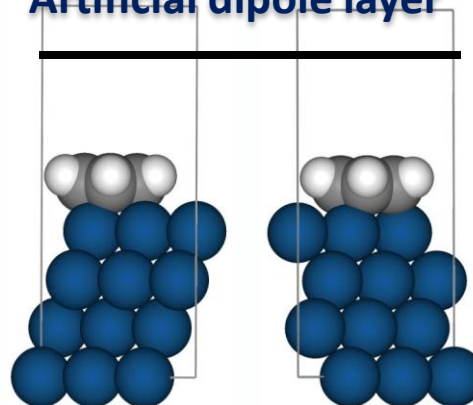
- ❑ Computational details:
 - ❑ PAW (Encut=400 eV)
 - ❑ 5 5 1 K-points
 - ❑ Methfessel Paxton, $\sigma=0.3$ eV
 - ❑ Non-spin polarized systems

Unit cell:



Top view

Artificial dipole layer



Side view

Vacuum layer 11 Å

Relax 2 upper layers

Fix 2 bottom layers

Statistical thermodynamics

□ DFT calculations provide:

- ❖ Electronic energy at 0 K from geometry optimization (E_{el})
- ❖ Vibrational frequencies from harmonic oscillator frequency analysis (ν)

Use of **statistical thermodynamics** to link between microscopic and macroscopic properties. Calculates the thermodynamic parameters as a function of T with the **partition function, $q(V,T)$**

$$q(V, T) = q_{elec}(T)q_{trans}(V, T)q_{rot}(T)q_{vib}(T) \quad q_{vib}(T) = \prod_{i=1}^{3N-6} \left(\frac{1}{1 - e^{-h\omega_i/k_B T}} \right)$$

Are the species **mobile** on the catalytic surface?

no

Immobile surface species

$$q_{rot}(T) = q_{trans}(V, T) = 1$$

yes

Mobile surface species

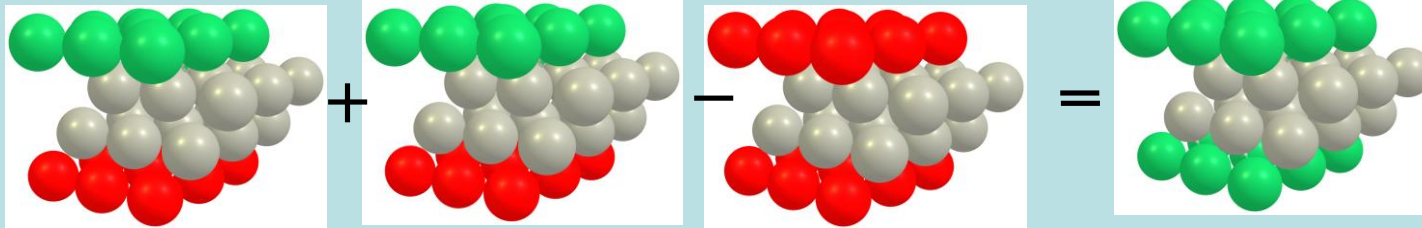
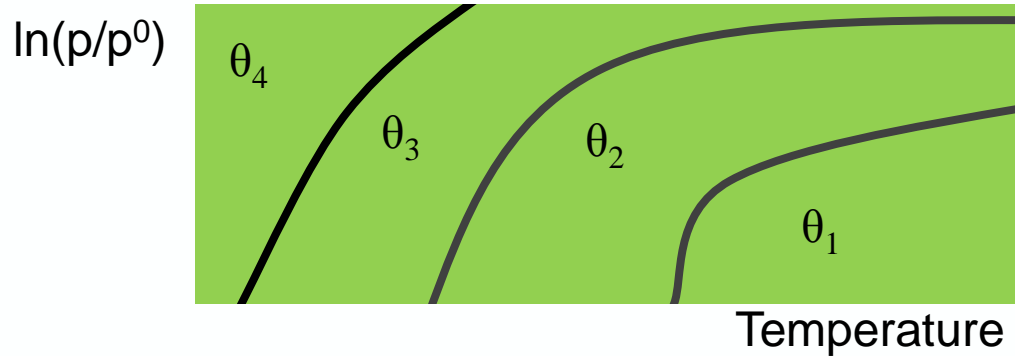
$$q_{mobile} = \frac{q_{immobile}^{vibr}}{q_{nD}^{vibr}} \times q_{nD}^{trans/rot}$$

- Free rotation
- Free translation

$$q_{rot} = \frac{8\pi^2 I k T}{h^2 \sigma}$$

$$q_{trans} = \left(\frac{2\pi M k T}{h^2} \right)^{3/2} V$$

Thermodynamic diagrams



Optimized surface

Non-optimized surface

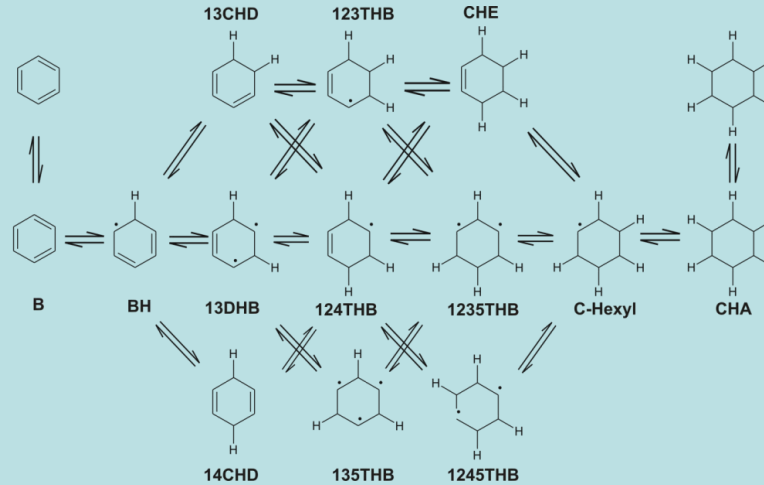
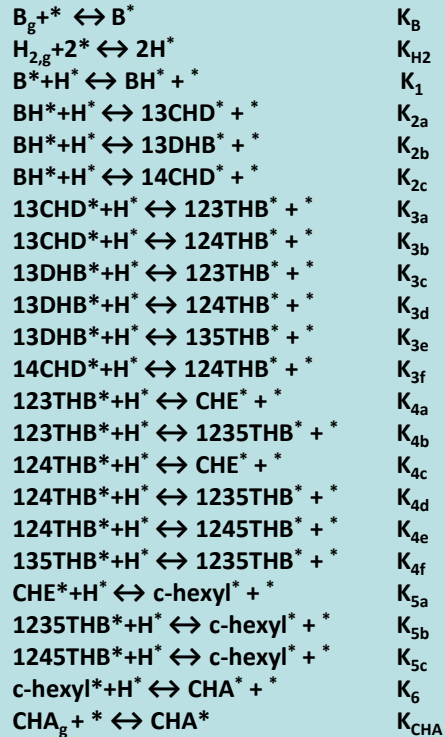
$$\Gamma_{0K,relaxed} = 2 \cdot \Gamma_{0K,opt} - \Gamma_{0K,non-opt} =$$

$$= 2 \times \left(\frac{E_{slab,opt} - n_{Pd,supercell} \times E_{bulk,opt} - \sum_i E_{i(g)} \times n_i}{2 \cdot A_{opt}} \right) - \left(\frac{E_{slab,non-opt} - n_{Pd,supercell} \times E_{bulk,non-opt}}{2 \cdot A_{non-opt}} \right)$$

$$\Gamma_{(T,P_i)} = \Gamma_{0K,relaxed} + \sum_i \frac{n_i}{N_a \times A} \times \left[T \cdot S_{i(T)}^0 - H_{i(T)}^0 + H_{i(0K)}^0 - R \cdot T \cdot \ln \frac{P_i}{P^0} \right]$$

Microkinetic modeling

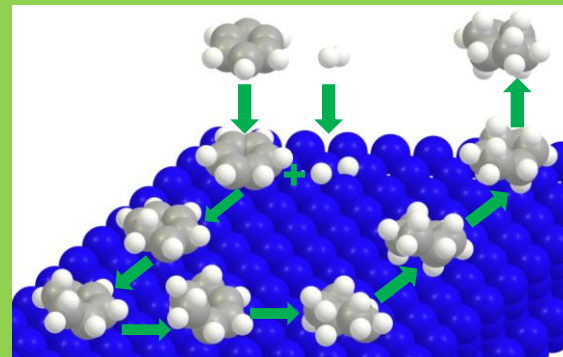
Full reaction network:



$$r = c_t \cdot (k_{des,CHA} \cdot \theta_{CHA} - k_{ads,CHA} \cdot p_{CHA} \cdot \theta_{CHA})$$

Dominant path with rate determining step

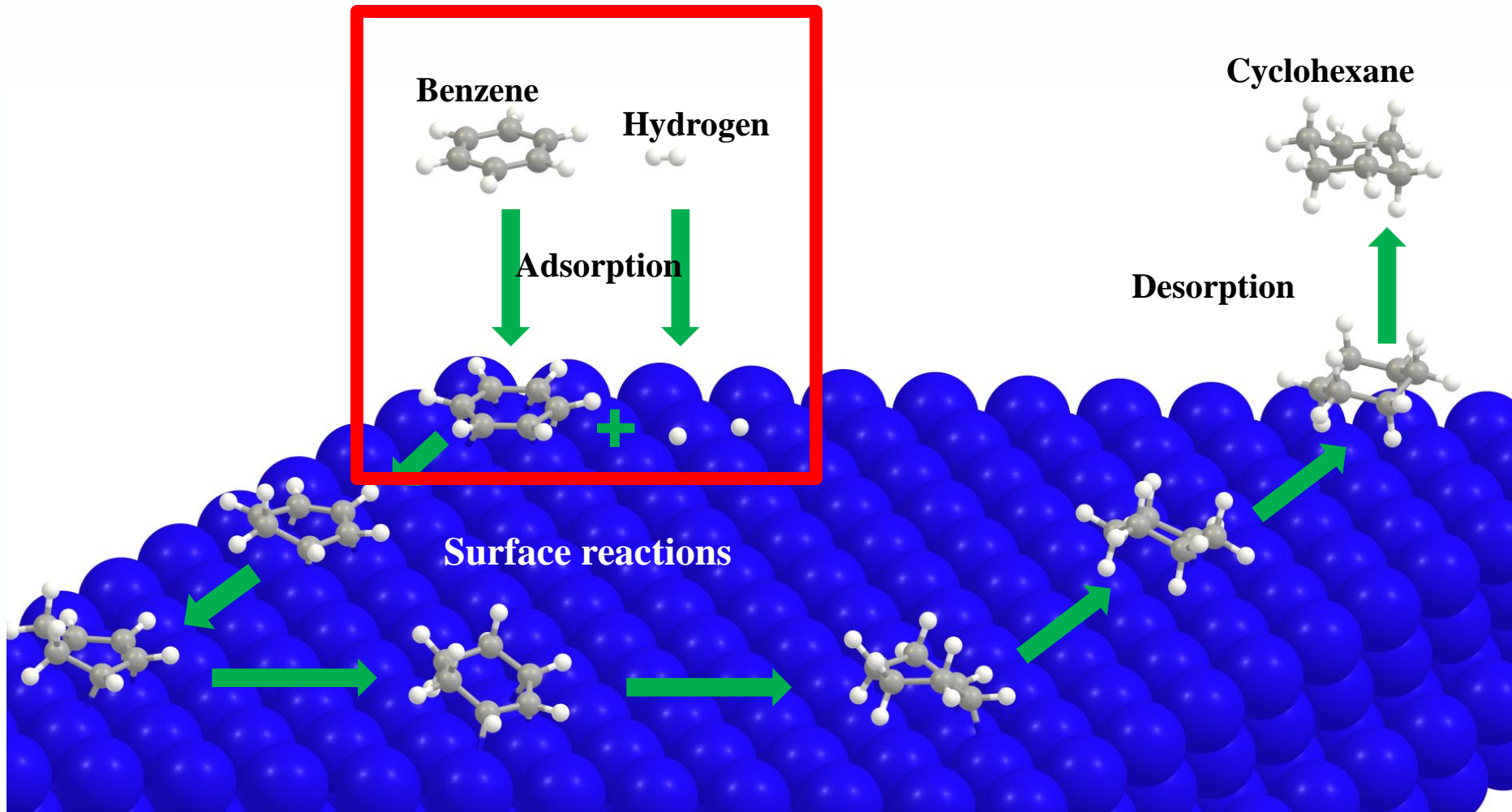
$$r = \frac{c_t \cdot k_{j(RDS)} \cdot \left(\prod_{i=1}^{i=j-1} K_i \right) \cdot K_B \cdot p_B \cdot K_{H_2}^j \cdot p_{H_2}^{\frac{j}{2}}}{\left(1 + K_B \cdot p_B + (K_{H_2} \cdot p_{H_2})^{\frac{1}{2}} \right)^2}$$



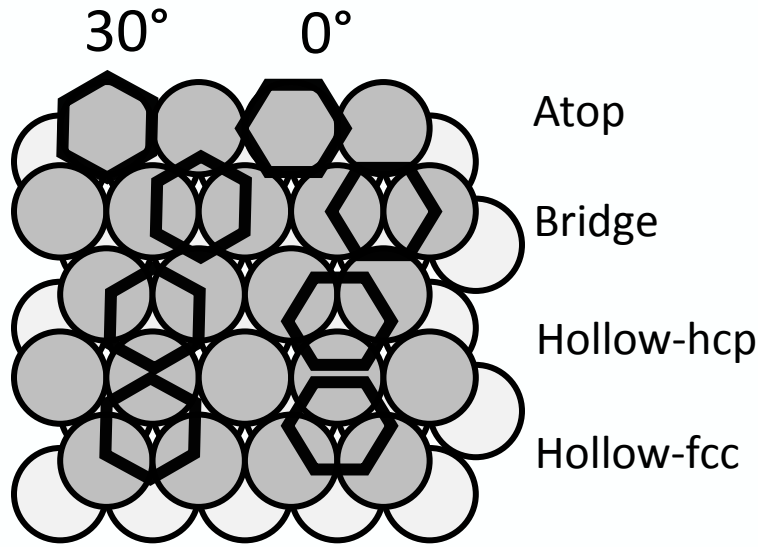
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- Introduction
- Methodology
- **Results**
- Conclusions

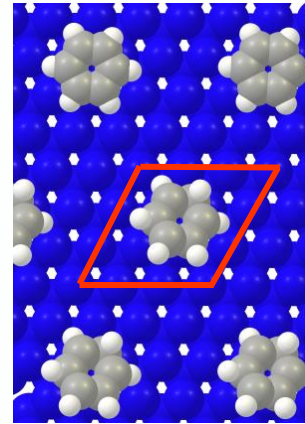
Results for the adsorption



Benzene adsorption

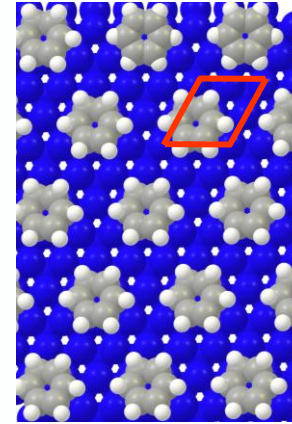


0.37 ML



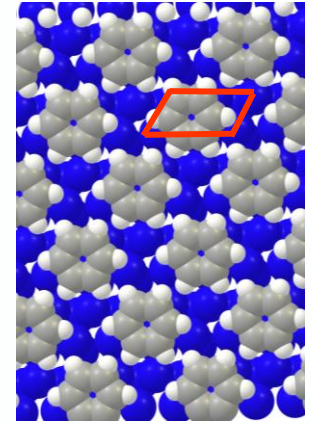
9.216×10^{13} molecules/cm²

0.67 ML



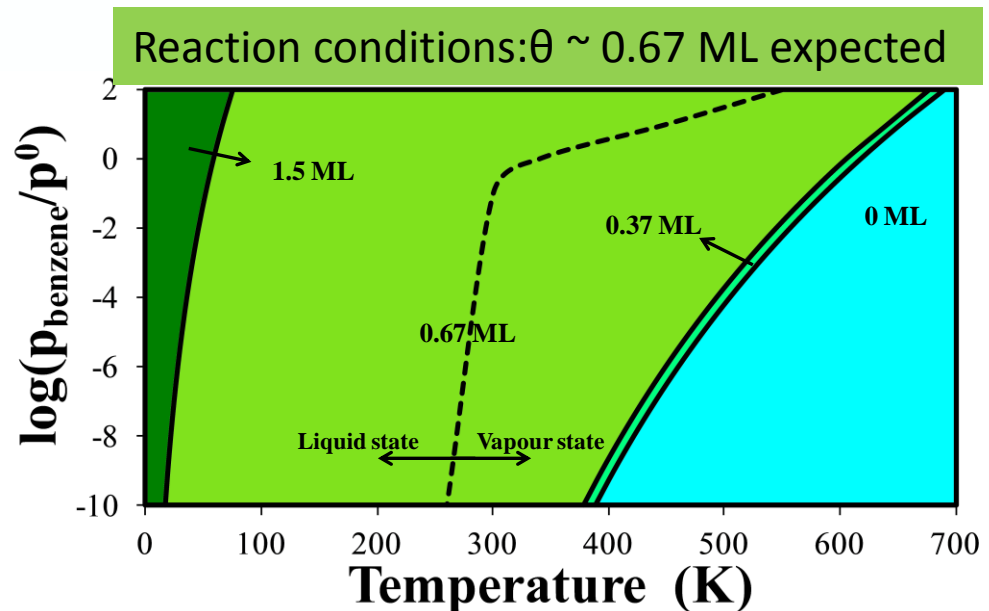
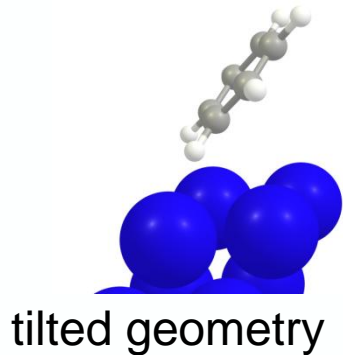
1.638×10^{14} molecules/cm²

1 ML



2.457×10^{14} molecules/cm²

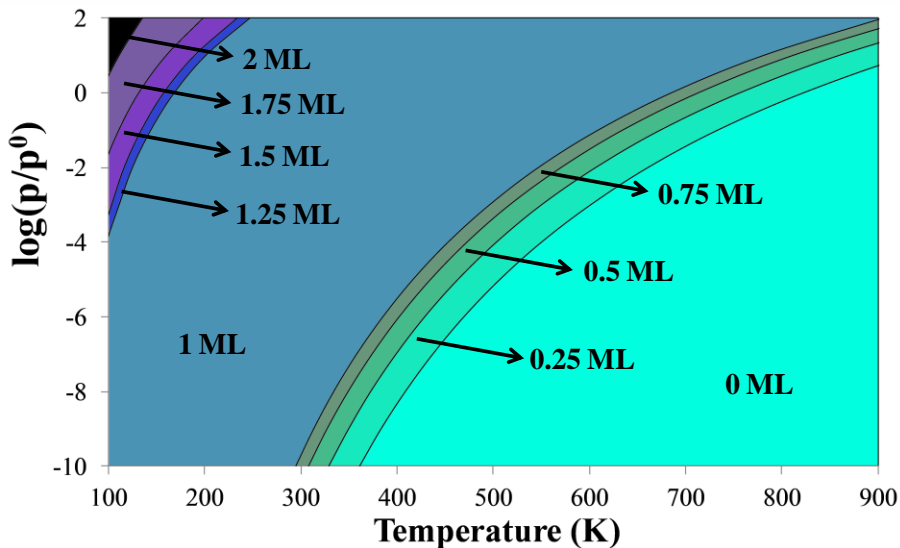
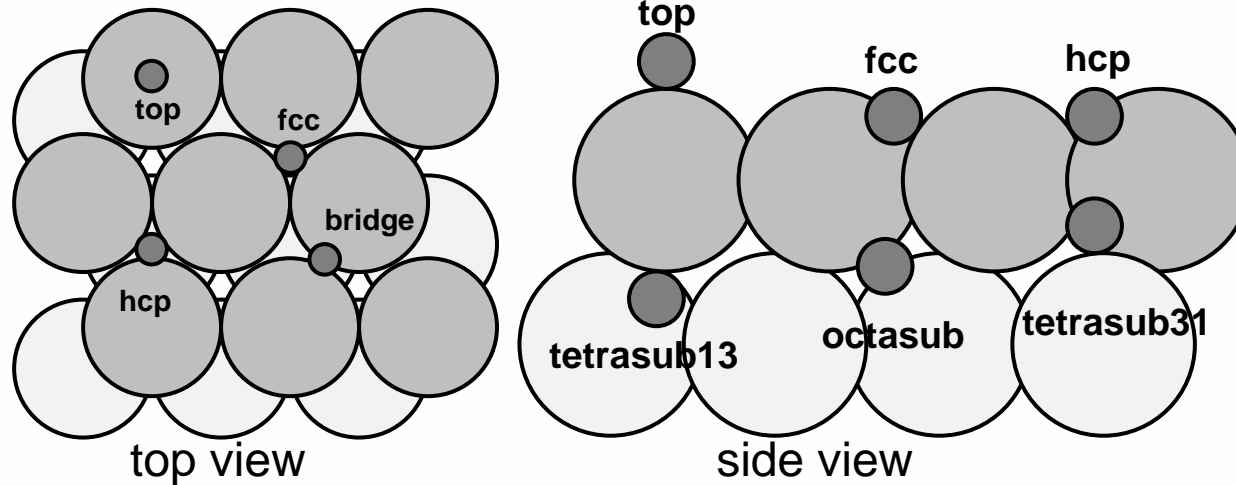
$\theta \leq 1$ ML: bridge30 and hollow-hcp0
 $\theta > 1$ ML: tilted configuration



Hydrogen adsorption

$\theta_H \leq 1\text{ML} \rightarrow$ Surface hollow sites

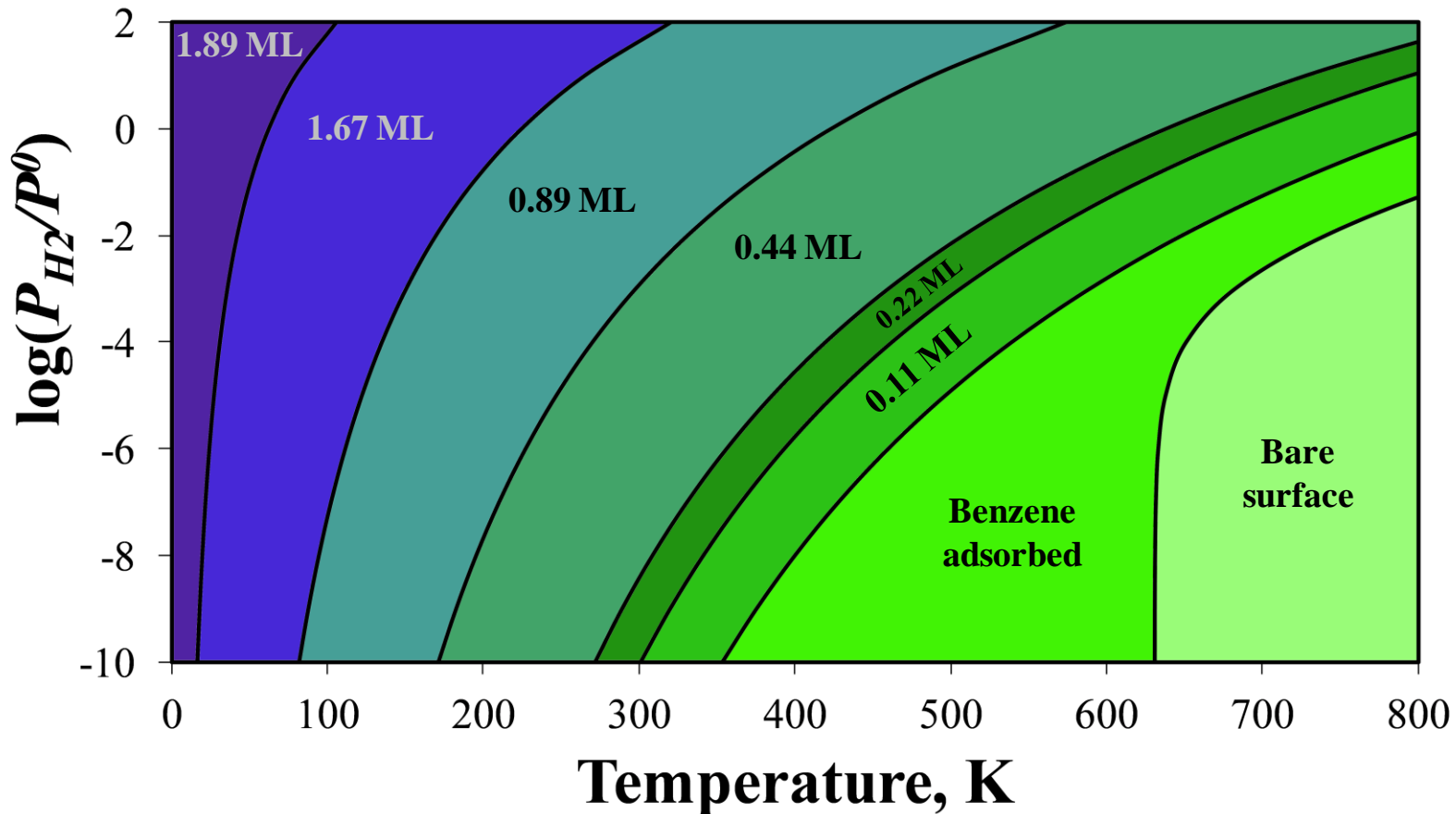
$1\text{ML} < \theta_H \leq 2\text{ML} \rightarrow$ Surf+Subsurface



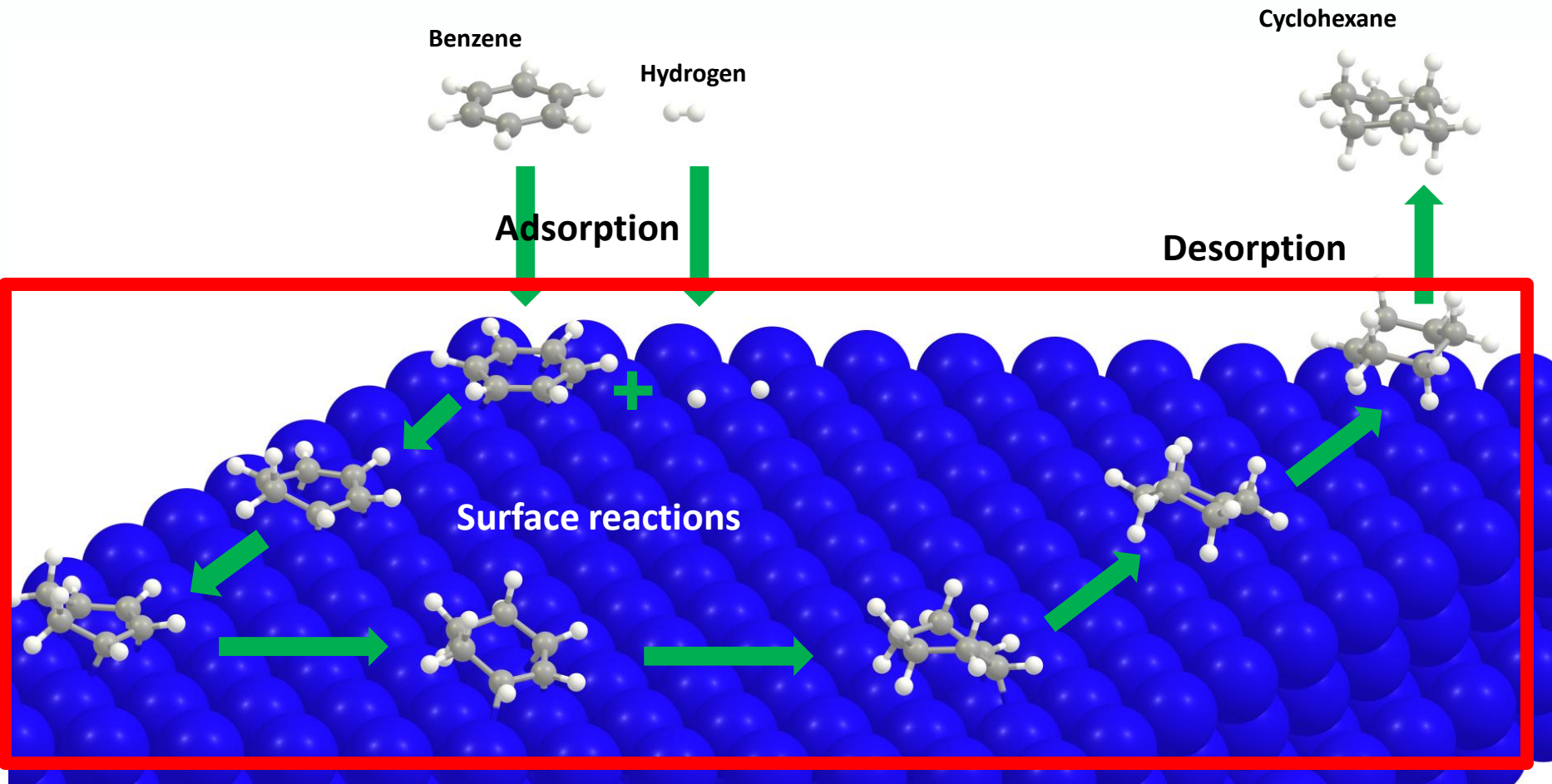
Hydrogenation conditions (450 K, >1 bar):
 $\theta_H \sim 1\text{ML}$ of surface hollow hydrogen

Benzene and hydrogen co-adsorption

Hydrogenation conditions (450 K, >1 bar):
 $0.44\text{ML} < \theta_{\text{H}} < 0.89\text{ ML}$ surface hydrogen

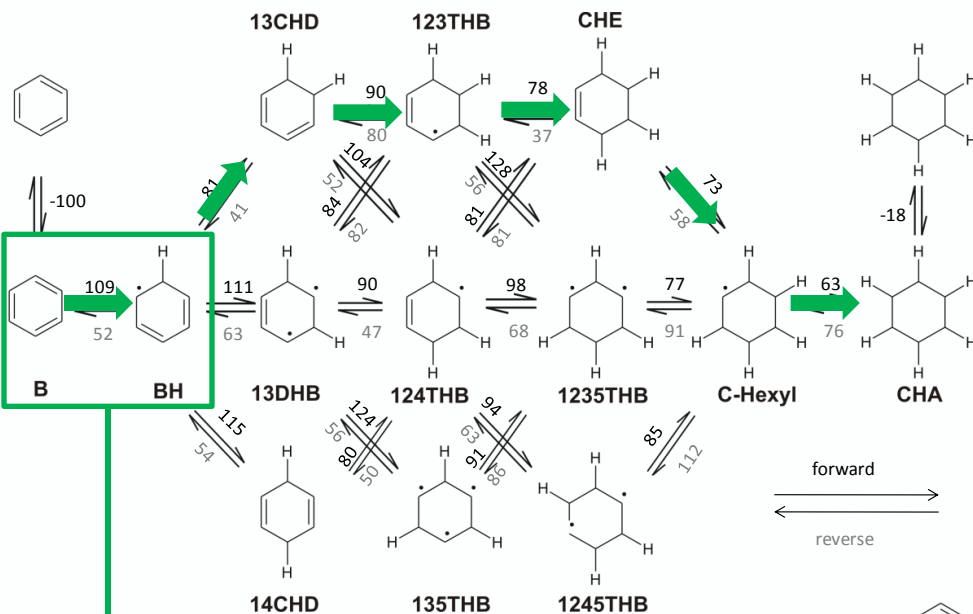


Results for the surface reactions



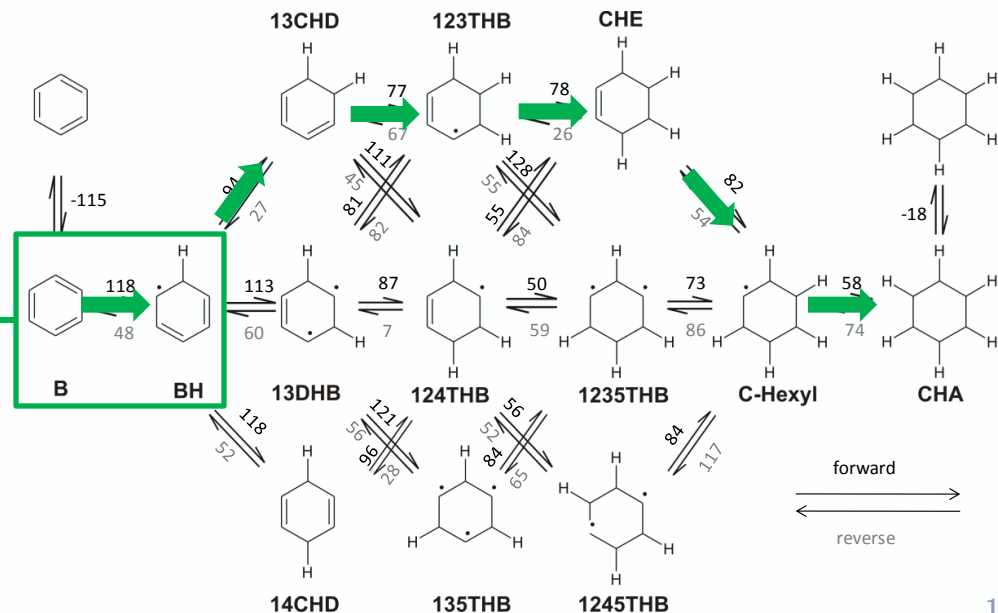
Electronic barriers for surface reactions

Hollow species

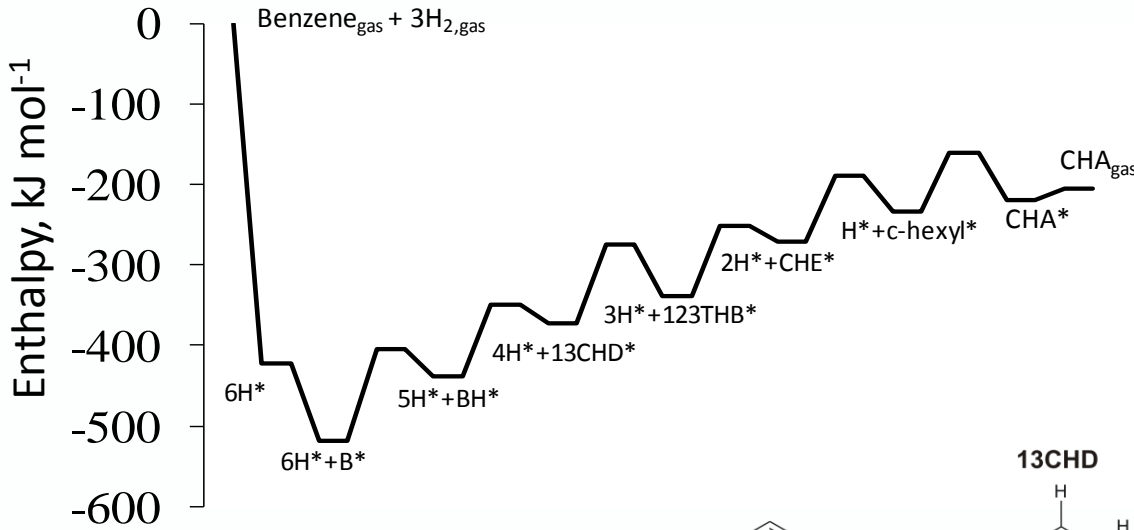


Potential rate determining step
 k_{RDS} strongly influences r

Bridge species



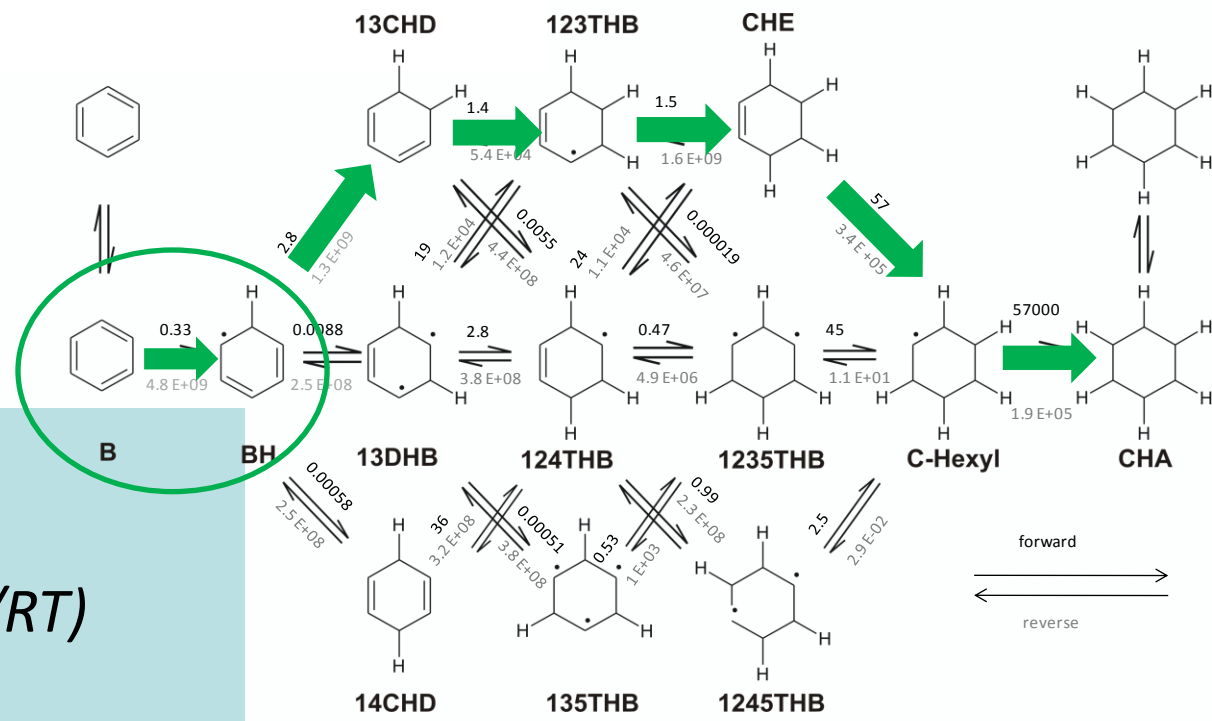
Thermodynamics & kinetics



Dominant path
 T=450K
 Hydrogen with free translation
 CHA free translation & rotation
 Cyclohexyl with free rotation

E_{el}, V
 q
 U
 H
 S
 ...

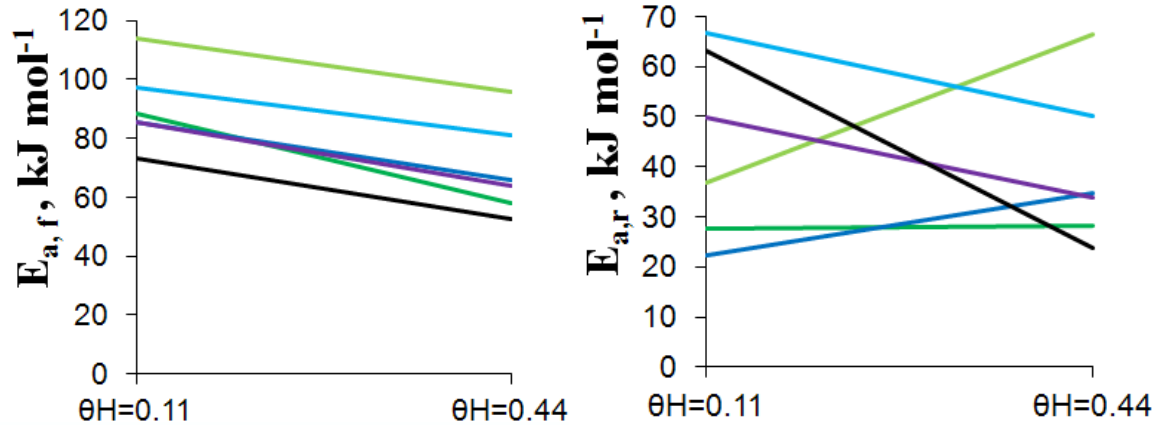
$A = f(S, T)$
 $E_a = f(H, T)$
 $k = A \exp(-E_a/RT)$
 $K = k_f/k_r$



Coverage dependent kinetics

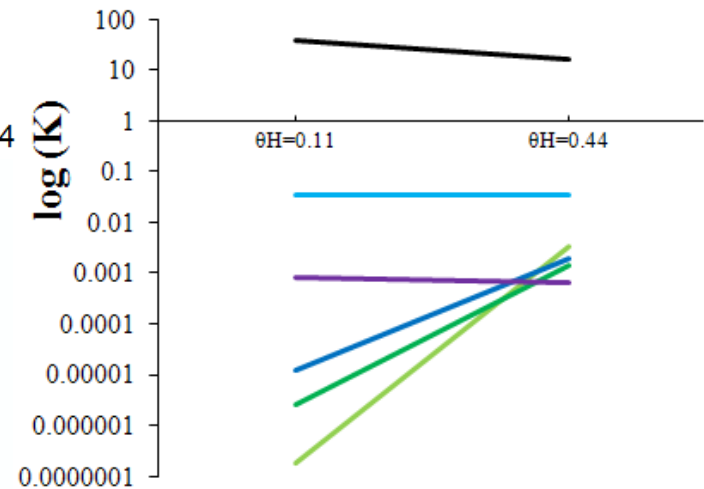
Dominant path evolution of kinetics with coverage, $0.11 \text{ ML} \leq \theta \leq 0.44 \text{ ML}$

Activation energy

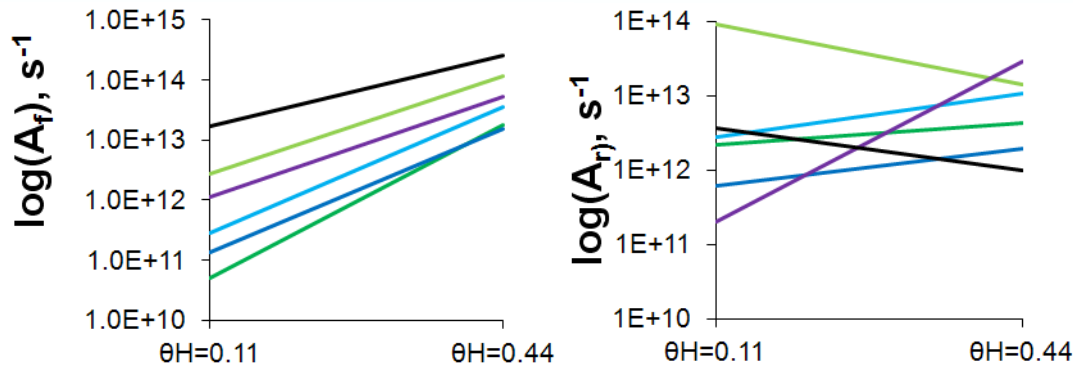


1st step
2nd step
3rd step
4th step
5th step
6th step

Equilibrium coefficient



Pre-exponential factor



Large increase in K_{eq} for
1st, 2nd and 4th reactions

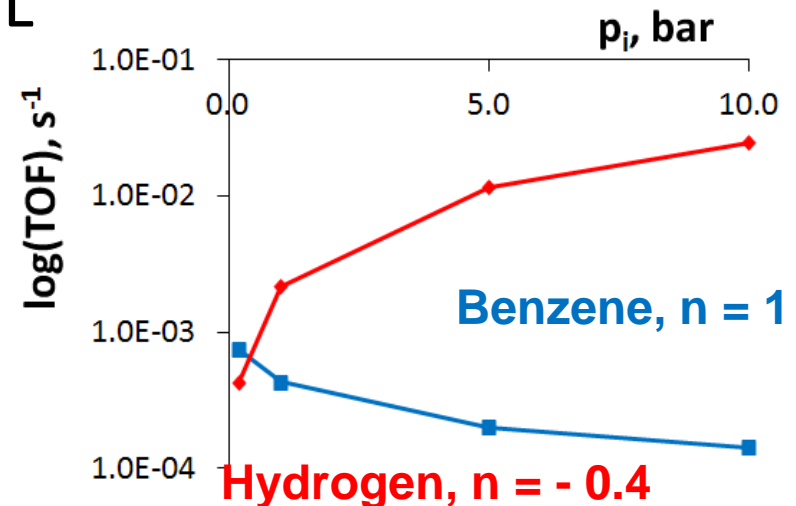
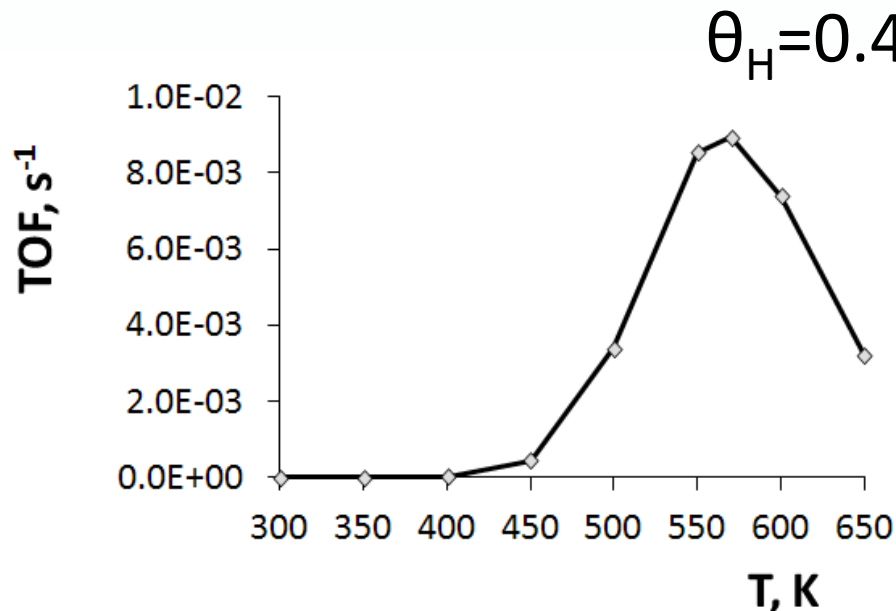
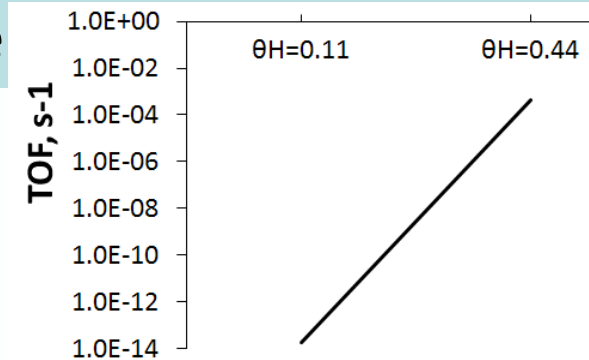
Coverage dependent kinetics

Higher hydrogen coverage:

- Decrease of E_a
- Increase of A
- Decrease of hydrogen mobility



Simulation of the microkinetics:
Large increase in TOF at high coverage



Outline

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Conclusions

Benzene adsorption on Pd(111):

- Flat up to 1 ML
- Tilted above 1 ML
- 0.67 ML preferred at reaction conditions

Hydrogen adsorption on Pd(111):

- Surface hollow sites up to ML
- Combination with subsurface above 1 ML
- 1 ML preferred at reaction conditions

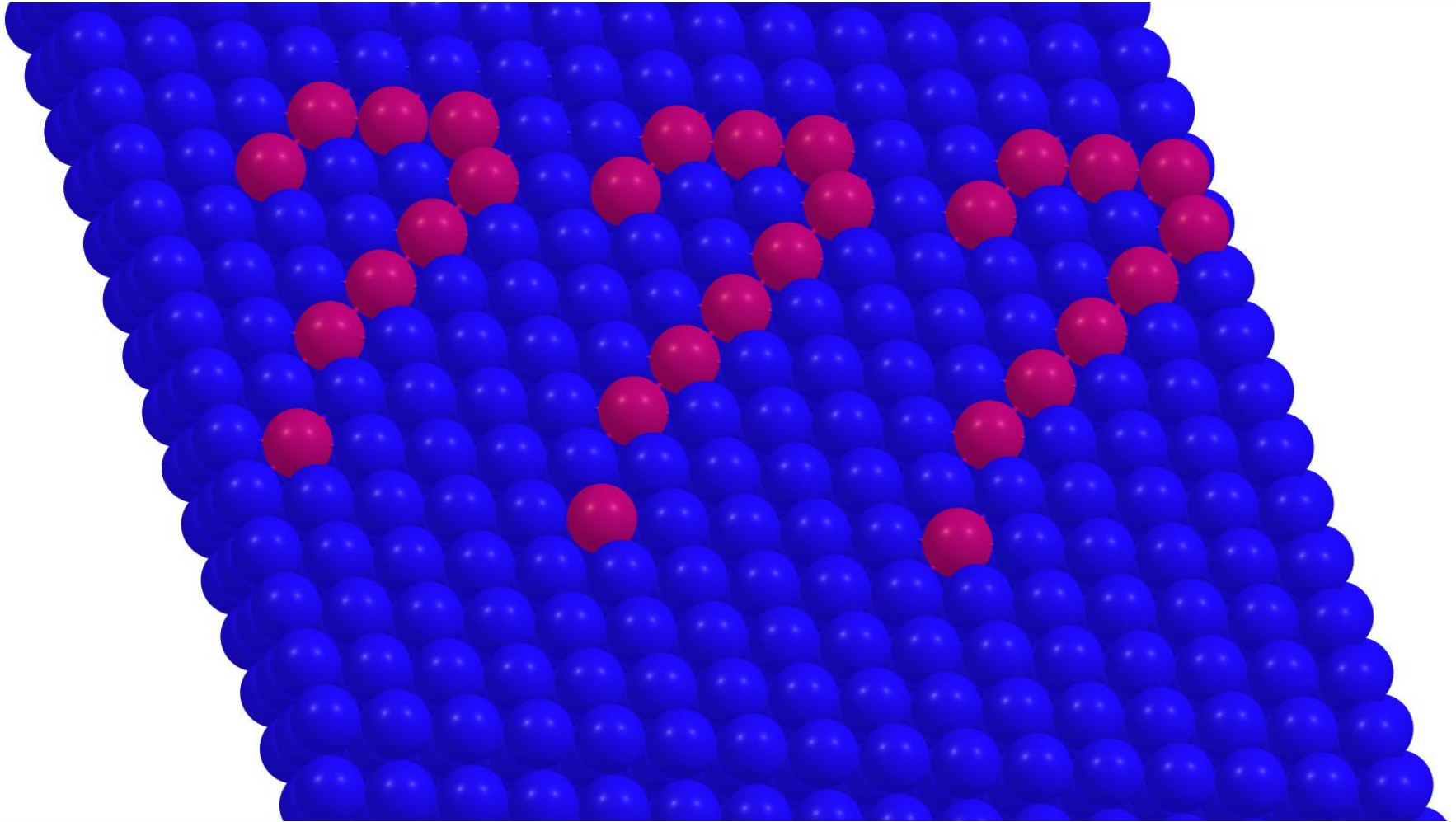
Co-adsorption on Pd(111):

0.44ML < θ_H < 0.89 ML surface hydrogen at reaction conditions, with 0.67 ML of benzene

Ab initio based micro-kinetics:

- Potential dominant path and rate determining step (upper path and first reaction resp.)
- Inclusion of coverage effects:
 - Decrease activation energies
 - Increase pre-exponential factor
 - Affect the mobility of hydrogen, which also impact on the kinetics
- Simulation of micro-kinetics shows much higher activities at high coverage
- Inclusion of hydrogen coverage effects improve the description of the reaction network

Thank you for your attention



Glossary

Catalyst descriptor: Characteristic for a given catalyst that can be correlated with kinetic and thermodynamic properties

DFT: Density Functional Theory

Dimer method: force-based transition state search algorithm

GGA: generalized gradient approximation (within DFT theory)

MEP: Minimum Energy Path

NEB: Nudged Elastic Band method for the calculation of MEPs

PAW: Plane Augmented Waves (periodic calculation technique)

PES: Potential energy surface

PW91: Perdew-Wang type of DFT functional

VASP: Vienna Ab initio Simulation Package

ZPE: Zero point energy