REALISTIC DYNAMIC BLOWER ENERGY CONSUMPTION MODELS FOR ACTIVATED SLUDGE SYSTEMS

Amerlinck, Y.¹, De Keyser, W.¹, Urchegui, G.², Maere, T.¹ and Nopens, I.¹

¹BIOMATH, Ghent University, Department of Mathematical Modelling, Statistics and Bioinformatics, Coupure Links 653, 9000 Gent, Belgium

Introduction

One of the main challenges for the optimization of activated sludge systems today is the proper evaluation of all important factors, for instance effluent quality (including priority pollutants), energy consumption and greenhouse gas emissions. At wastewater treatment plants (WWTPs) aeration is the largest energy consumer (Ast et al. 2008, Devisscher et al. 2006, Fenu et al. 2010, Tchobanoglous et al. 2004, Zahreddine et al. 2010). As such aeration energy consumption is an essential factor to be considered in the optimization of activated sludge systems. Despite the increasing level of detail in wastewater treatment process models, oversimplified energy consumption models (i.e. constant "average" power consumption) are being used in optimization exercises (Copp 2002, Gernaey et al. 2006, Martín de la Vega et al. 2013, Rosso and Stenstrom 2005, Wambecq et al. 2013). As these models have the interesting potential to be used in multi-criteria optimization exercises (e.g. optimizing effluent quality, greenhouse gas emissions and operational costs simultaneously), they may lead to poor predictions and their use in optimization could lead to suboptimal operation. Therefor the authors propose a new, dynamic model, based on the same principles as the one they previously successfully applied for pumping applications (De Keyser et al. 2014).

A new dynamic model for a more accurate prediction of aeration energy costs in activated sludge systems, equipped with submerged air distributing diffusers (producing coarse or fine bubbles) connected via piping to blowers, has been developed to overcome this unbalance in the coupled submodels. The objective of the proposed model is to allow for dynamically simulating the power consumed by an aeration system in function of (a) the physical characteristics of the aeration system (i.e. blowers, piping, diffusers), (b) the water height in the aerated tanks and (c) the volumetric air flow rate imposed by a control system. The poster will illustrate that the dynamic model is preferably used in optimisation efforts for energy minimisation.

Materials and methods

Key factors that influence WWTP aeration cost are the type of aeration blower employed, the aeration system configuration (e.g. diffuser types, water head and piping characteristics) and the control strategy implemented on the aeration system. The blowers employed in fine bubble diffuser aeration systems are compressors operating at low relative pressures and can be classified into two broader classes, i.e. centrifugal and positive displacement (PD) types (Henze et al., 2009). To date, three main control strategies are implemented to enable "turn-up" or "turn-down" capacity to these aeration blowers, namely variable Inlet Guide Vane (IGV) control, Outlet Throttling (OT) control and Variable Frequency Drive (VFD) control.

Key issues to be considered when evaluating the energy consumption of aeration systems are: (1) energy requirement for compression, (2) inlet conditions of the air, (3) system characteristic curve, (4) blower characteristic curve, (5) blower efficiency and (6) the type of process control strategy employed.

² MONDRAGON SISTEMAS, S. COOP. (MSI), AmaKandida, 21 DENAC, 20140 Andoain(Gipuzkoa) Spain

Results and discussion

The developed model will be further explained in the poster. The model is demonstrated for the aeration system at the Mekolalde WWTP (originally designed to treat wastewater of 40,000 PE) located in Bergara (Guipúzcoa, Spain). This system uses a positive displacement blower (PD blower Mapner SEM.40TR). After calibration the model proved to give an accurate prediction of the real energy consumption by the blowers (Figure 1). Comparison was made with constant average power consumption (a fixed ratio power consumption over flow rate) models and it was shown (Figure 2) that the dynamic model captures the trends better than the constant average power consumption.

Conclusions

A new dynamic model for a more accurate prediction of aeration energy costs in activated sludge systems, equipped with submerged air distributing diffusers (producing coarse or fine bubbles) connected via piping to blowers, has been developed and demonstrated. The new model proved to give an accurate prediction of the real energy consumption by the blowers and captures the trends better than the constant average power consumption models currently being used. This clearly illustrates, also because the cost of energy depends on peak demand values, that the dynamic model is preferably used in multi-criteria optimization exercises for minimizing the energy consumption.

References

Ast, T., DiBara, M., Hatcher, C., Turgeon, J. and Wizniak, M.O. (2008) Benchmarking Wastewater Facility Energy Performance Using ENERGY STAR® Portfolio Manager. Proceedings of the Water Environment Federation 2008(8), 7322-7339.

Copp, J.B. (2002) The COST simulation benchmark—description and simulator manual, Office for Official Publications of the European Communities, Luxembourg.

De Keyser, W., Amerlinck, Y., Urchegui, G., Harding, T., Maere, T. and Nopens, I. (2014) Detailed dynamic pumping energy models for optimization and control of wastewater applications. Journal of Water and Climate Change (Under Revision).

Devisscher, M., Ciacci, G., Fe, L., Benedetti, L., Bixio, D., Thoeye, C., De Gueldre, G., Marsili-Libelli, S. and Vanrolleghem, P.A. (2006) Estimating costs and benefits of advanced control for wastewater treatment plants - the MAgIC methodology. Water Science and Technology 53(4-5), 215-223.

Fenu, A., Roels, J., Wambecq, T., De Gussem, K., Thoeye, C., De Gueldre, G. and Van De Steene, B. (2010) Energy audit of a full scale MBR system. Desalination 262(1-3), 121-128.

Gernaey, K., Nopens, I., Vrecko, D., Alex, J. and Dudley, J. (2006) An updated proposal for including further detail in the BSM2 PE calculation, [internal BSM2 taskgroup document].

Martín de la Vega, P.T., Jaramillo, M.A. and Martínez de Salazar, E. (2013) Upgrading the biological nutrient removal process in decentralized WWTPs based on the intelligent control of alternating aeration cycles. Chemical Engineering Journal 232(0), 213-220.

Rosso, D. and Stenstrom, M.K. (2005) Comparative economic analysis of the impacts of mean cell retention time and denitrification on aeration systems. Water Research 39(16), 3773-3780.

Tchobanoglous, G., Burton, F.L., Metcalf, Eddy and Stensel, H.D. (2004) Wastewater Engineering: Treatment and Reuse, McGraw-Hill.

Wambecq, T., Fenu, A., De Gussem, K., Parmentier, G., De Gueldre, G. and Van de Steene, B. (2013) The impact of horizontal water velocity on the energy consumption of a full-scale wastewater treatment plant. Water and Environment Journal 27(2), 247-252.

Zahreddine, P., Dufresne, L., Wheeler, J., Couture, S., Reardon, D. and Henderson, K. (2010) Energy Conservation Measures for Municipal Wastewater Treatment Innovative Technologies and Practices. Proceedings of the Water Environment Federation 2010(13), 3359-3384.

Figures and tables

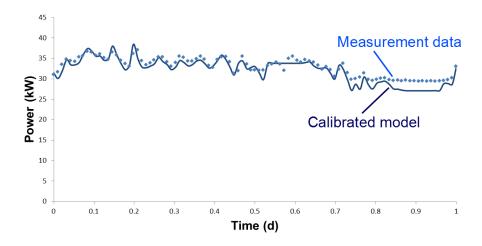


Figure 1. The calibrated dynamic model (dark blue line) show a close fit to the measurement data (blue dots), including the trends.

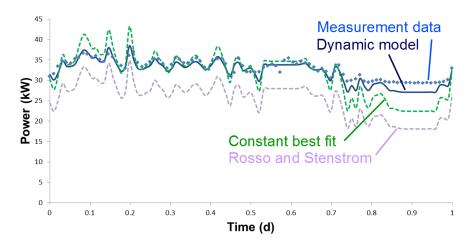


Figure 2. The dynamic model (dark blue line), describes the measurement data (blue dots) and its trends better than the models with constant average power consumption ratios. Both the model by Rosso and Stenstrom (2005) (purple dashed line) and the model with the best fit for the average of the data (green dashed line) show larger variations.